

Research and Development

DEVELOPMENT OF PROPOSED

STANDARD TEST METHOD FOR

SPRAY PAINTING TRANSFER EFFICIENCY

Volume II. Verification Program

Prepared for

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Prepared by

Air and Energy Engineering Research Laboratory Research Triangle Park NC 27711

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DEVELOPMENT OF PROPOSED STANDARD TEST METHOD FOR SPRAY PAINTING TRANSFER EFFICIENCY

VOLUME II. VERIFICATION

PROGRAM

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ABSTRACT

Over the past 5 years, the Environmental Protection Agency Air and Energy Engineering Research Laboratory has been working to develop a standardized laboratory test method for determining the transfer efficiency of spray painting operations. This document describes the final phase of laboratory experiments conducted to characterize the interlaboratory precision of the transfer efficiency test method developed in earlier efforts.

The test program included extensive experiments conducted at eight industrial spray painting laboratories. Three types of spray equipment (conventional air spray, electrostatic air spray, and airless) were tested at each laboratory. Six replicate transfer efficiency measurements were made for each equipment type at each laboratory.

The results of these experiments document the maturity of the draft standard transfer efficiency test method and the expected ruggedness of the results to differences within and between laboratories. As anticipated from earlier research efforts, the transfer efficiency results for each spray system were different. However, the results for each spray system demonstrated exceptional consistency when expressed as within-laboratory standard deviation. (Standard deviation is expressed in units of transfer efficiency. It can be used for estimating precision at various confidence intervals.) The within-laboratory standard deviation across eight laboratories was:

Conventional air spray 1.52 Electrostatic air spray ... 1.91 Airless spray 1.10

These within-laboratory standard deviations clearly demonstrate the capability of the test method to produce consistent results within a particular laboratory. The within-laboratory standard deviations were well below the value predicted at the onset of this project, 2.5.

The total standard deviations were considered from two standpoints. The first standpoint included the deviations directly attributable to differences among the spray guns used for the tests. These values were based on the total variance, including the within-laboratory portion of the variance (shown in the table above), gun-to-gun portion of the variance, and between-laboratory portion of the variance. The total standard deviations are reported below.

Conventional air spray 6.79 Electrostatic air spray ... 9.42 Airless spray 5.82 The second standpoint included the within-laboratory portion of the variance and the between-laboratory portion of the variance. However, it excluded the gun-to-gun portion of variance (that is, the part attributable directly to differences among the spray guns). The total standard deviation (excluding gun-to-gun differences) are presented below.

Conventional air spray ... 6.72 Electrostatic air spray ... 8.70 Airless spray 5.26

The exclusion of the gun-to-gun portion of the variance marginally improves the total standard deviation.

While arguments can be made towards including and excluding the gun-to-gun differences in the overall analysis, it makes little impact on the results of this study. Between-laboratory variances accounted for the vast majority of the total standard deviation for all equipment types at all ranges of transfer efficiency observed.

For the convenience of the reader, total standard deviations are referred to in this report as either <u>including gun differences</u> or excluding gun differences.

In classical interlaboratory programs there are two measures of the quality of the method: accuracy and precision. Precision is the measure of variability. The precision goals and results of this research have been discussed above and are presented in detail herein. Accuracy is the measure of how far off the observed values of transfer efficiency are from the true transfer efficiency. In this research there is no known true measure of transfer efficiency; therefore, accuracy cannot be addressed. However, since accuracy is a measure of the bias encountered in estimating the value of a parameter (and because there is no reason to believe that we have a significant bias for the spray system, laboratories, and targets examined), it is believed that the draft transfer efficiency test method is reasonably accurate. The absence of evidence regarding bias may be interpreted as an absence of bias.

TABLE OF CONTENTS

Abstract
List of Tables
Abbreviations and Symbols vi
1. Introduction
2. Conclusions and Recommendations
3. Background
4. Phase I - Airless Transfer Efficiency Test Method
5. Phase II - Design of Interlaboratory Experiments
6. Performance of Experiments
Test Site l
Test Site 2
Test Site 3
Test Site 4
Test Site 5
Test Site 6
Test Site 7
Test Site 8
7. Test Results and Statistical Analysis 5
Appendices
A Proposed Standard Transfer Efficiency Test Method A-
B Quality Assurance/Quality Control Plan B-
C Detection of Outliers by Means of Nalimov's Test . C-
D Statistical Analysis Addendum D-
E Operating Conditions and Raw Data Summary E-

LIST OF TABLES

		Page
5-1	Level of Support Required from Participating Laboratories	11
5-2	Paint Specifications	17
6-1	Order of Airless Gun Testing	24
6-2	Order of Electrostatic Air Spray Gun Testing	26
6-3	Order of Conventional Air Spray Gun Testing	27
6-4	Laboratory l Test Results	28
6-5	Laboratory 2 Test Results	32
6-6	Number of Laboratories (b) Required to be P% Sure that the Estimated Total Variance is Within K% of the True Value	35
6-7	Laboratory 3 Test Results	37
6-8	Laboratory 4 Test Results	40
6-9	Laboratory 5 Test Results	43
6-10	Laboratory 6 Test Results	47
6-11	Laboratory 7 Test Results	50
6-12	Laboratory 8 Test Results	53
7-1	Transfer Efficiency Results, % Transfer efficiency, Airless	55
7-2	Transfer Efficiency Results, % Transfer efficiency, Conventional air spray	56
7-3	Transfer Efficiency Results, % Transfer efficiency, Electrostatic air spray	57
7-4	Transfer Efficiency Results	5.8

ABBREVIATIONS AND SYMBOLS

LIST OF ABBREVIATIONS AND UNIT CONVERSIONS

ABBREVIATIONS

AOAC -- Association of Official Analytical Chemists ASTM -- American Society for Testing and Materials
EPA -- United States Environmental Protection Agency

Fan air -- shaping air or horn air
FP -- flat panel (target configuration) PSIG -- pounds per square inch, lb/in², gauge

O&M -- operating and maintenance

QA/QC -- quality assurance/quality control

VOC -- volatile organic compounds

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SECTION I

INTRODUCTION

Spray painting transfer efficiency is a measurement of that quantity of paint solids which actually coats a surface compared with the total paint solids sprayed. Transfer efficiency measurements can be used to optimize on-line spraying or to develop more efficient spray equipment. More recently, the need to determine transfer efficiency has taken on a new aspect: transfer efficiency can be used to quantify volatile organic compound emissions from spray painting operations.

During the past 5 years, the U.S. EPA has been conducting extensive research on transfer efficiency. The objective of this research has been to develop a laboratory transfer efficiency measurement method. Many companies have developed their own methods for determining efficiency; however, these methods vary widely in capability although most share common elements. The EPA research program was designed and initiated to develop the necessary background and research data to permit development of a standardized laboratory transfer efficiency test method. To ensure as broad participation in the program as possible, numerous sources in the industry were contacted and their assistance solicited where possible.

Earlier research developed a laboratory transfer efficiency measurement method. The approach used was to develop the test method by studying concepts for transfer efficiency determination and methods currently in use and then using the best features of each. Laboratory tests were conducted to provide supporting data and to establish the precision of the formulated method. The tests established the standard deviation (repeatability) of the transfer efficiency results as less than 2.5 within a given laboratory. (Standard deviation is always expressed in the units being measured by the test. In this research it is always expressed in units of transfer efficiency.)

The research program described in this document was conducted to establish the efficiency of the transfer efficiency method using the preliminary draft method defined earlier in this program. Eight field-based laboratories participated in this test program. Electrostatic air spray, conventional air spray, and airless spray systems were tested at each laboratory.

SECTION 2

CONCLUSIONS AND RECOMMENDATIONS

The preliminary draft transfer efficiency test method was used at eight laboratories. Within each participating laboratory the results were repeatable at levels well below the standard deviation goal of 2.5 set by previous research (CENTEC Corporation, 1982).

A statistical analysis of the results showed that the gun portion and the within-laboratory portion of the total variance were small. The between-laboratory portion of the variance was over six times larger than the within-laboratory portion of the variance. This ratio implies that the differences between laboratories were real and resulted in detectable, quantifiable differences in transfer efficiency that can be attributed to differences between participating laboratories.

The toal standard deviations observed from laboratory to laboratory ranged from 5.82 (airless spray) to 9.42 (electrostatic spray). The preliminary results of this research indicate that the probability that the transfer efficiency measured at a random qualifying laboratory would fall within 7.3 to 12.0 transfer efficiency units of the true transfer efficiency, provided that the assumption that bias is nil is correct.

These results must, however, be considered preliminary. A sufficient number of laboratories was not used in the program to comply with an 80 percent probability criteria to establish for method precision.

SECTION 3

BACKGROUND

The EPA has been attempting to develop regulatory strategies to control the emissions of VOC from metal coating processes of the metal finishing industry. In those processes where the emission streams are easily defined and contain relatively high concentrations of VOC, development of regulations has been straight-forward. Those regulations are based primarily upon the ease with which presently available control technologies can be used to control high VOC concentration emission streams. Those technologies include carbon adsorption and incineration.

Although high concentration emission streams can be controlled effectively with available technologies, as VOC concentrations decrease the available control system's economic and technical feasibility also decreases. Questions have also been voiced by representatives of industry and government about the relationship of various metal coating techniques to their VOC emissions potential.

To date no method has been certified as a standard to measure transfer efficiency. Numerous companies and technical organizations, however, have proposed methods for measuring transfer efficiency. These have yet to be shown to have sufficient precision and accurary to define transfer efficiency for most painting scenarios. Thus, transfer efficiency measurements have not become a part of present control strategies for compliance with VOC emissions regulations. Only when a simple yet accurate and precise method of measuring painting transfer efficiency is developed can TE be used in VOC control strategies.

Beginning in 1982, a contract was authorized by EPA to develop a preliminary transfer efficiency test method. Laboratory studies and evaluations were conducted to define a procedural method to accurately and precisely measure transfer efficiencies from various spray painting equipment. This equipment included

conventional air spray, electrostatic air spray, and rotating bell spraying equipment. Results of these studies are presented in Volume I.

The current project was conducted in two parts. The first part addressed the status of the transfer efficiency method for airless spray equipment, which was not researched during previous phases of this program. The second part involved the implementation and validation testing at multiple laboratories to estimate the precision of the transfer efficiency test method.

SECTION 4

PART I - AIRLESS TRANSFER EFFICIENCY TEST METHOD

In the first part of this contract, background information on existing methods for determining the transfer efficiency of airless spray painting equipment was developed. Information from publicly available sources was obtained through a manual and computer literature search. A wide spectrum of private industry sources was contacted, including major spray painting equipment manufacturers, industrial metal finishers and spray painters, and paint formulators. These sources were questioned about different methods for determining the transfer efficiency of airless equipment. The general consensus was that there were no characteristics unique to airless spray which would make the current test method unacceptable except the need to determine mass flow with a meter rather than using scales and a stopwatch. In airless spraying, the paint pot is connected via high pressure hose to a reciprocating pump. This connection, and the action of the pump, make the scales vibrate. vibration can be severe enough to make reading the scales difficult if not impossible.

Preliminary test results of the transfer efficiency procedure defined in appendix A, found that a reasonable degree of precision could be achieved. The standard deviation of replicate flat panel target test runs using airless spray guns was 1.31 and the standard deviation of replicate vertical cylinder test runs was 0.03, both well within the range of 2.5 that was specified in the preliminary draft test procedure. Therefore, it was concluded that the existing draft transfer efficiency test method was appropriate for airless spraying equipment even though it was not as well developed as for other spray painting systems.

To document this conclusion, a conventional airless spray system was selected as one of the three spray equipment types to be used for the second part of this study. The selection of airless spray equipment also helped to ensure that the preliminary draft transfer efficiency test method would be thoroughly developed across a wide range of transfer efficiencies.

SECTION 5

PART II - DESIGN OF INTERLABORATORY EXPERIMENT

PROGRAM DESIGN

The purpose of the experimental strategy of this effort was to build an interlaboratory test program that allowed estimation of the precision of the draft standard transfer efficiency test method. For this purpose, no operating parameters were intentionally varied during the program.

The strategy was divided into four major components: establishing the number of laboratories for the test program, deciding what equipment types were to be tested at each laboratory, estimating the number of replicates to be made for each equipment type at each laboratory, and establishing the gun portion of the variance. The experimental strategy called for replicate transfer efficiency determinations to be made at each laboratory participating in the program. These determinations were to be made using the same type of equipment (in similar condition) at the same spray conditions (controlled and held constant as provided in the QA/QC plan in Appendix B). These conditions were established during the first laboratory experiment and were held constant for all subsequent laboratory experiments in this program. Equipment operating conditions were set at the first laboratory to provide a good spray pattern and reasonable finish. The spray environment (i.e., the configuration of the laboratory, proximity of grounds, airflow patterns, and so forth) necessarily was less controlled from laboratory to laboratory than were the spray conditions. Ideally, interlaboratory method verification experiments would be conducted at nearly identical laboratories using identical spray equipment and identical operating conditions. However, from a practical standpoint it is impossible to have 100 percent identical laboratories. Thus, it might be expected that the resulting transfer efficiency valves will be somewhat different between laboratories.

ESTABLISH THE NUMBER OF LABORATORIES

The number of laboratories required to determine the precision of a test method within certain estimated confidence limits may be estimated from existing data generated from the same analysis performed at different laboratories. In this program, however, the existing data base could not be used for estimation of the number of laboratories because previous data were not obtained at the same conditions. Known and quantifiable differences existed between transfer efficiency tests conducted at four different laboratories under prior research efforts. Further, other documented transfer efficiency determinations performed by industry could not be documented as meeting required project QA/QC plans; their results also could not be used to estimate the number of laboratories required.

The results of transfer efficiency determinations made during this program at the same laboratories as prior studies could not be compared to the results of the prior research. The spray equipment, paint system, and operating conditions for this program were not the same as for prior efforts; thus, the results are not comparable. They are from different sets.

Since previous data were obtained at inconsistent spray painting conditions, an experimental design was undertaken that was not dependent upon prior data and was most efficient of resources. The experimental methodology meeting these criteria was the sequential experimental design. In the planned sequential experimental design, the same test was conducted at two laboratories. The data from these two laboratories served as a basis for further sample size projection. The results from these two laboratories truly reflected the most current level of knowledge.

Appropriate computations of number of laboratories required were made from the transfer efficiency results of the first two laboratory tests. The data from the first two test laboratories served as a portion of the final data set to be analyzed. This approach was consistent with the current trend in the field of experimental design, i.e., design the experiment in stages, using preliminary stages to make decisions regarding design parameters for the final stage (Steinberg and Hunter, 1984). This sequential experimental design allowed the program to avoid relying too heavily on the use of preliminary data that might be suspect or incompatible with the conditions anticipated in this study.

Based on the preliminary calculation described above, it was expected that this sequential methodology would result in selection of approximately eight laboratories for testing in the interlaboratory program. (The number of laboratories participating under this contract was fiscally limited to eight.) This estimate was also based on recommendations of the American Society for Testing and Materials in their Standard Practice for Conducting an Interlaboratory Test Program to Determine the Precision of Test Methods (ASTM E 691-79, Part 41). This estimate was further supported by the Association of Official Analytical Chemists in their statistical manual (Steiner and Youden, 1975).

Selection of laboratories for participation in this program was based primarily upon the availability of necessary facilities; this selection process was necessarily assumed to be random for purposes of the statistical analysis.

ESTIMATE THE NUMBER OF REPLICATES

The number of replicates (n) for each gun type must be sufficient to reduce the variance of the test precision to an acceptable value. In this program, parameters were chosen for an 80 percent

confidence interval that the total variability would be within a certain range. In that confidence interval, the element that drives down the total variability is the number of laboratories. The number of replicates at each laboratory (based on within-laboratory estimates of precision from previous experimental data) is not as important. As shown in the equation below, the total variance (excluding gun variance, which is addressed separately) is much more sensitive to the number of laboratories than to the number of replicates.

$$\sigma_{\rm T} = \frac{2\sigma_{\rm w}^4}{b\,({\rm n-1})} + \frac{2\,(\sigma_{\rm w}^2 + 2\,(\sigma_{\rm \bar{b}}^2)^2)}{n\,(b-1)}$$

where

 σ_{T} = total variance (excluding gun variance)

 $\sigma_{\mathbf{W}}$ = within laboratory variance

 $\sigma_{b}^{"}$ = between-laboratory variance

n = number of replicates at each laboratory

b = total number of laboratories

Based on this equation, one can see that changing the number of replicates from six to ten hardly affects the confidence interval, while increasing the number of laboratories from six to seven shrinks the confidence interval significantly.

Six replicates were considered adequate to meet this criterion based on previous experiments. Thus, six replicate transfer efficiency measurements were made for each equipment type in each laboratory under equivalent conditions for equivalent equipment types, as best as could be controlled.

ESTABLISH EQUIPMENT TYPES FOR TEST PROGRAM

Although the precision of the test method may be estimated by testing a single spray system across a number of independent laboratories, this approach would leave some questions as to the consistency of interlaboratory precision over a wide range of transfer efficiencies. It was important to establish that the test method was as precise at low transfer efficiencies as it was for high transfer efficiency values. To avoid this question, three spray types (having a wide range of anticipated transfer efficiency values) were selected for this research. system types were electrostatic air spray, conventional air spray, and airless. As documented in prior research (cited above), electrostatic air spray and conventional air spray painting systems typically have considerably different transfer efficiencies even when operating in the same booth, using the same test paint and targets. For instance, during testing conducted in June 1983, conventional air spray equipment exhibited transfer efficiencies ranging from 10

percent to 60 percent, while electrostatic air spray equipment exhibited transfer efficiencies from 75 percent to 95 percent. Both spray systems used the same test paint, in the same spray booth, with the same sets of target configurations.

Electrostatic air spray and conventional air spray systems operate on different principles: conventional air spray equipment relies on the paint particle size and mass velocity to carry it to the desired target, while electrostatic air spray equipment uses an electrical attraction in addition to conventional attractive forces to draw the paint to the desired target. These differences make the selection of electrostatic air spray and conventional air spray systems desirable for this research. It allowed demonstration of the ruggedness of the test method to different spray mechanisms across a number of laboratories.

An additional advantage of selecting electrostatic air spray and conventional air spray equipment was that equipment costs were minimized. As recommended by the Spray Painting Transfer Efficiency Project Steering Committee in March 1985, electrostatic air spray equipment was used both as electrostatic equipment and to simulate conventional air spray equipment by turning off the electrostatics. In fact, these types of spray equipment (as offered by one manufacturer) were virtually identical except for the electrode on electrostatic spray guns. The decision to simulate conventional air spray equipment by using electrostatic air spray with the electrostatics turned off saved over \$5,200 in equipment costs. It resulted in further savings by eliminating the amount of time needed to change equipment types (twice) at each laboratory.

A third equipment type, (conventional) airless, was also included in the test program as a result of Part I recommendations. Airless spray equipment does not have the test history of other equipment types. In order to ensure that the test method was as well developed for airless spray equipment as it was for other equipment types, airless equipment was included in this test program.

Automatic guns were recommended by the Spray Painting Transfer Efficiency Project Steering Committee, since they had not been fully tested using the draft standard transfer efficiency test method; however, automatic spray equipment was not available within the time frame and budget available for this program. Manual spray equipment was used for all tests in this program. The spray guns were fixed in position using a mounting pole, and were triggered manually with the exception of an actuator (automatic triggering device) used at one laboratory on the manual spray guns.

ESTABLISH THE GUN PORTION OF THE VARIANCE

By nature, the interlaboratory test program involved almost simultaneous testing at up to eight sites. This requirement necessitated the use of different spray guns (of the same make and model) from laboratory to laboratory. It was desirable to know the portion of the between-laboratory variance that was due strictly to differences in spray guns. This variance is called the "gun-to-gun portion of the variance" or "gun portion of the variance." The gun portion of the variance was considered part of the between-laboratory variance; it is never possible to test the identical gun at identical conditions at two laboratories. Even the same gun would have undergone additional wear in the process of being tested.

The gun portion of the variance had to be established to determine whether it was significant and, if so, to determine what portion of the total variance it represented.

The gun portion of the variance was established during the first laboratory test. Eight different spray guns (of same make and model) for each equipment type were subjected to replicate transfer efficiency determinations at the same laboratory. (These same guns were used in subsequent laboratory tests in this program.) Six replicates were conducted for each gun. The data were analyzed to determine how much difference in transfer efficiency was attributable to using different guns.

At the first test, mean transfer efficiencies and standard deviations from each of the three sets (one set for each equipment type) of 48 transfer efficiency determinations (eight guns per equipment type multiplied by six replicates for each gun) were compared. The gun portion of the variance was derived as described in Section 7 - Test Results and Statistical Analysis.

LABORATORY REQUIREMENTS AND SELECTION

Spray painting laboratories were required to meet certain minimum criteria in order to participate in the interlaboratory test These criteria included their ability to provide the laboratory conditions and support listed in Table 5-1, their willingness to participate in a timely manner, their laboratory rental cost, and their level of interest in the project. Best professional judgment and previous test experience were used to determine which laboratory conditions could reasonably be controlled from test to test. The Steering Committee contributed to defining laboratory conditions for testing. Part of the between-laboratory variance, then, accounted for uncontrollable differences from laboratory to laboratory. If more laboratory conditions had been specified (such as relative humidity), or condition ranges had been more closely defined (such as booth air rate at 95-105 fpm instead of 80-120 fpm), no known laboratories would have qualified to perform the test. Laboratory selection

TABLE 5-1. LEVEL OF SUPPORT REQUIRED FROM PARTICIPATING LABORATORIES

- o Two technicians, knowledgeable and proficient with spray system use and maintenance (minimum)
- o Back-draw water wash spray booth or equivalent, with 80-120 fpm air velocity in middle at plane of target (if dry filter booth is used, laboratory must provide sufficient filters to maintain these conditions), associated chemicals and operating costs
- o Adjustable speed (20 to 40 fpm) overhead conveyor system capable of hanging EPA targets as specified
- o Conveyor speed measurement equipment
- o Utilities
- o Paint mixing equipment and facilities for documenting paint characteristics (contractor provided Ford viscosity cup)
- o Curing oven of sufficient size for curing EPA targets, with temperature control at 375°F
- o Curing rack
- o Timer
- o Cleaning solvents
- o Packing and shipping to next facility
- o Air rate measurement equipment
- o Humidity and temperature measurement equipment
- o Foil cutters
- o Foil handling facilities
- o Laboratory scales (0.001g accuracy)
- o Hangers for targets
- o Compressed air supply in laboratory
- o Temperature control in laboratory (65 75°F)
 Relative humidity was recorded but could not be controlled at available laboratories.
- o Spray equipment assembly tools

TABLE 5-1. LEVEL OF SUPPORT REQUIRED FROM PARTICIPATING LABORATORIES (Continued)

- o Copying machine (for completed data sheets)
- o Work space for record keeping and calculations
- o Security for test equipment and supplies
- o Miscellaneous hose and fittings

was assumed to be random within the defined sample frame, although there was no absolute method to confirm the assumption.

Participating laboratories were required to supply at least two knowledgeable and conscientious technicians for the test program. Technicians were required to be familiar with the test equipment and capable of performing the tests precisely, as described in the Test Plan supplied to each laboratory.

In previous testing it was found that the transfer efficiency was influenced by the linear booth air velocity. In order to have consistent results, it was necessary to control the air velocity as much as possible. At the suggestion of the Spray Painting Transfer Efficiency Project Steering Committee, it was decided that a qualifying air rate of 100 fpm + 20 fpm at the plane of the target in the center of the booth would be required for all participating laboratories.

An adjustable speed overhead conveyor system, a curing oven, and hangers large enough to handle the EPA targets were required to be supplied by the laboratories. The EPA targets consisted of ten 15.24 cm (6 in) wide metal panels mounted 15.24 cm (6 in) apart, and hanging 121.9 cm (48 in) in length (see Volume I). The importance of an adjustable speed overhead conveyor system can not be overemphasized because it provided the means to control the speed of the targets passing through the spray area. Since the conveyor speed is a controlled parameter, it necessitated the need to have conveyor speed measurement equipment at each participating laboratory. The degree of sophistication required was such that using a stopwatch and timing marks was an acceptable measurement method as allowed in the procedure.

Because this testing involved a standard test method, measurement and/or control of other pertinent parameters was essential. The temperature of the testing area could affect the Transfer efficiency and therefore was controlled to within a few degrees centigrade (that is, +5°F). Air rate measurement equipment (anemometer), humidity measurement equipment, and laboratory scales with 0.00lg accuracy were included as part of the level of support needed from participating laboratories.

Finally, all interested laboratories were required to have paint mixing equipment, cleaning solvents, foil handling facilities, miscellaneous hose and fittings, spray equipment assembly tools, and a copying machine available during the testing period. Utilities, including compressed air and electricity, were also required.

EPA and its representatives, and cooperating equipment manufacturers and suppliers, supplied other test equipment, including but not limited to spray painting equipment and auxiliaries, test method, data books, and technical guidance.

The laboratories agreed that none of the test equipment supplied would be used for any purpose other than was directly related to the EPA transfer efficiency research program. This agreement specifically forbade using, tampering, dismantling, or otherwise examining this equipment except as required for the test program or for proper maintenance. An appropriate amount of security was necessary to ensure that this requirement was enforced.

Each laboratory was required to allow EPA representatives and EPA contract engineers full and complete access to the test area. The laboratories agreed to allow Spray Painting Transfer Efficiency Project Steering Committee members into their facility as observers of the research program.

Suitably equipped industrial laboratories were recommended through the Spray Painting Transfer Efficiency Steering Committee, through outside listings of available laboratories (Thomas' Register of Manufacturers, state-by-state industrial directories, Products Finishing 1984 Directory, and Metal Finishing Guidebook and Directory and Metal Finishing Guidebook and Directory for 1984.)

Participating laboratories were asked to schedule two weeks each for conducting tests except in the case of the first test, which required four weeks of laboratory time. Several additional experiments were conducted during the first test.

TEST EQUIPMENT

Overview of Test Equipment

In this part of the program, three types of spray equipment were tested at up to eight laboratories. One spray equipment type, electrostatic air spray, was used to simulate conventional air spray equipment as well. Thus, two complete spray systems were obtained for electrostatic air spray and for airless. Eight spray guns of the same make and model were obtained for use on the two electrostatic air spray and two airless systems. equipment types are described in detail below. Spray systems and guns were supplied to participating laboratories in new condition to ensure as nearly identical spray equipment conditions as possible. Each component of the spray system, from the gun tip to hoses and supply tanks, was required to be of the same size, make, and model. This requirement enhanced control of variances from spray system to spray system. Each spray gun was mounted in the proper spray position on a pole. Spray gun operation was manual (hand-triggered), except at one laboratory where a remote actuator was employed.

Other test supplies and equipment described in this section include instrumentation, paint, targets, and foil. The supply of some test equipment was required of participating laboratories. These were described earlier in this section.

Electrostatic/Conventional Air Spray Equipment

A manual mid-range (75 kV) electrostatic air spray gun was selected for use as electrostatic spray equipment and to represent conventional air spray equipment. (As previously described, the same equipment was used but without voltage applied.) The electrostatic air spray gun was equipped with a 1.2 mm (0.047 in) fluid tip. This was the same model spray gun used during a previous test effort conducted to determine how operating and maintenance variables affect transfer efficiency (U.S. EPA, 1985). It was considered representative of manual electrostatic air spray guns available from other manufacturers, although differences exist from manufacturer to manufacturer.

A 75 kV adjustable power supply was used to support the electrostatic air spray gun. This is a mid-range power supply equipped with appropriate cable and connections. A kV meter and ammeter were built into the power supply control panel. Power cables were supplied in 762 cm (25 ft) lengths for each power supply.

Pressure tanks were used to supply paint to the gun through 1524 cm (50 ft) fluid lines. A dual air regulator pressure tank with agitator (to minimize stratification of the paint) was supplied with each electrostatic air spray system. Air hoses were supplied in 1524 cm (50 ft) lengths for each system.

Airless Spray Equipment

A manual airless spray gun was selected for the interlaboratory test program. The spray gun included a 0.38 mm (0.015 in) diameter tip.

An electric pump was the fluid supply mechanism. The small, 1.89 liter per minute (0.5 gpm) pump was used. Fluid hose was obtained in 762 cm (25 ft) lengths for airless transfer efficiency determinations. Two fluid hoses were used in each test, with one segment spanning from the pump to the control panel (see below) and one segment spanning from the control panel to the spray gun.

Instrumentation

Control Panel

Two control panels were constructed to provide adequate process control equipment to participating spray painting laboratories. Each control panel housed air and fluid regulators, an air rotameter, a mass flow meter, and a mass flow totalizer on a movable cart. The regulators had a pressure range of 6.9 to 344.7 kPa (1 to 50 psig). The recommended supply pressure for the regulators was 827.3 kPa (120 psig), with a maximum supply pressure of 1034.2 kPa (150 psig). All connections were 1/4 NPT.

Five pressure gages were mounted in each control panel. These pressure gages monitored air and fluid pressure throughout the spray system. All gages were dead-weight calibrated prior to testing. Dead-weight calibration is a standard method for calibrating pressure gages by applying a static ("dead") pressure. In this case, a series of static pressures (framing the expected test pressures) were applied to each gage being calibrated. Calibration curves were developed and used for all gages used in this research.

A direct scale reading rotameter was included on each control panel to indicate air flow through the system.

A mass flow meter was utilized to indicate the total mass of paint sprayed during each test. Each control panel was equipped with a mass flow meter. This meter was fitted with a digital totalizer, enabling test personnel to read paint mass flow quickly and easily.

Other Instrumentation

An anemometer was available to laboratories not having their own equipment to document the spray booth air velocity.

A sling psychrometer was also available to laboratories not having their own relative humidity or thermal measurement equipment.

A calibrated #4 Ford viscosity cup was supplied for use at each laboratory.

Paint

Certain desirable paint characteristics were necessary for the test program. The same paint was to be sprayed by all spray systems, except that the viscosity of the paint was higher for airless spray equipment. Thus, the paint had to be of relatively high viscosity when uncut but mid-range viscosity when cut. It had to have a simple solvent system, for ease in obtaining and simplicity in cutting (thinning) at test sites. The paint had to be readily available from a large manufacturer's batch to encourage homogeneous characteristics. It had to adhere well to aluminum foil without cracking, peeling, or breaking. It was required to have at least a 6-month shelf life so that a single batch could be used in all experiments in this program. Paint resistivity must be high for electrostatic spraying, or the paint may ground the system. Finally, the paint had to be reasonably priced and readily available.

The selected paint met these criteria as summarized in Table 5-2. It was a highly flexible alkyd base paint commonly used for painting light fixtures. As shown in Table 5-2, the paint was cut to a wide range of viscosities using xylol. Nitration grade xylol was used as the solvent.

Supplier: Glidden 447-W-02133

Resistivity: 360 Megohms/cm

Nonmetallic

Alkyd based

Xylol solvent (titration grade)

Part of a high volume batch

Adheres well to aluminum foil

Cure: 900 s (15 min) at 190.5°C (375°F)

Approximately 52 percent solids by weight, after cutting

A sample of the test paint was sent to the first laboratory for field confirmation of its properties. It met all test requirements.

During the tests, paint weight percent solids were determined several times daily as required by the test method and by the project QA/QC plan (Appendix A and Appendix B, respectively). ASTM Method D-2369, Standard Test Method for Volatile Content of Coatings, was used for all paint weight percent solids determinations, except that the vendor-recommended cure schedule was followed.

Foil

A medium-temper aluminum alloy foil was required by the draft transfer efficiency test method (Appendix A). As described in the test method, 0.0037 cm (1.5 mil) thick foil, 38.1 cm (15 in) wide and on rolls approximately 21336 cm (700 ft) long, was supplied to participating laboratories by the contractor. Over 227 kg (500 lbs) of foil was supplied to test laboratories, or about 28.4 kg (62 lbs) per laboratory.

Targets

As directed by the draft transfer efficiency test method, one EPA target consisted of a set of ten galvanized steel 121.9 cm (48 in) by 15.2 cm (6 in) panels mounted on 30.48 cm (12 in) centers (see Appendix A). A set of ten panels thus configured and hung on an adjustable speed conveyer was used for each transfer efficiency determination. The first two and last two panels in

each set of ten were scavengers. Selection of these targets over other configurations is discussed later in this section.

Twelve sets of targets (consisting of ten panels each) were supplied to each participating laboratory to help expedite transfer efficiency testing. By having extra targets on hand, one member of the research team could be weighing and wrapping panels in preparation of testing while other researchers were setting up spray equipment. During testing, as each spray painting pass was completed and the targets removed for curing, another set of prepared targets was ready for mounting and spraying.

Targets were suspended so that the spray pattern fell across the middle of the target, with a minimum 30.5 cm (1 ft) clear space between the edge of the spray pattern and the target top and bottom. This requirement was to prevent excessive overspray. Previous transfer efficiency test results using target configurations ranging from large flat panels (almost prohibiting overspray) to small vertical cylinders hung on wide centers (almost totally overspray) demonstrated that either extreme design tended to desensitize the transfer efficiency test method. That is, target configuration affected the ability of the test method to detect changes in transfer efficiency. The target configuration selected for this research was determined to be the most sensitive target type tested. Therefore, the selected target configuration was most likely to detect changes in transfer efficiency within or between laboratories.

SECTION 6

PERFORMANCE OF EXPERIMENTS

FIRST LABORATORY

Special tests were conducted at the first laboratory in this program. First, base spray conditions were established for each type of equipment. Once established, these conditions were used for all subsequent transfer efficiency determinations in this program. Second, the gun portion of the variance was established through a prescribed set of experiments. Finally, the first interlaboratory test was conducted.

The draft transfer efficiency test method (Appendix A) was used for all transfer efficiency determinations made in this program. The test method as presented in Appendix A has been modified to include base spraying conditions from the first laboratory as part of the test criteria. These criteria were a necessary part of the interlaboratory test program, and are not part of the generic draft transfer efficiency test method.

Establish Base Spray Conditions

Prior to conducting transfer efficiency determinations at the first laboratory, standardized spray conditions were established. (These same conditions were used at all subsequent laboratories.) Spray conditions were established through a trial-and-error procedure to determine an acceptable spray pattern and finish. Extensive previous transfer efficiency testing using the same types of spray equipment and similar paint was used in setting the first rough approximations of spray conditions and in adjusting conditions. Disposable paper targets were used for the rough first approximations of spray conditions. Foil-covered EPA targets were painted at tentative spray conditions to demonstrate their appropriateness for use with the actual test targets.

Of the spray conditions, paint viscosity was one of the hardest to set and control. Paint viscosity was to be set at mid-range (15 s on a #4 Ford cup) for electrostatic air spray and conventional air spray transfer efficiency determinations. Paint viscosity was set at 30 s on a #4 Ford cup for airless spraying. Nitration grade xylol was used to cut the paint to specified conditions. ASTM D-1200-70 was the method used to determine paint viscosity.

Test booth conditions were documented prior to setting spray conditions and prior to conducting transfer efficiency determinations. If booth conditions did not meet test requirements, or if process control systems (booth rate, regulators,

mass flow meter, etc.) were not operating, they were repaired prior to setting spray conditions.

Actual spray system operating conditions were set for airless equipment first. Gun-to-target distance, fluid pressure, and paint viscosity adjustments were set at manufacturer's recommendations. Test patterns were shot onto paper and operating conditions were adjusted until a good spray pattern was realized. Once a good spray pattern was realized, foil-covered EPA targets were painted and cured. When the resulting coating was acceptable, spray operating conditions were documented. These spray conditions were fixed for the remainder of airless equipment testing in this program.

Airless testing for gun portion of the variance and for the first interlaboratory test was conducted at base operating conditions.

Electrostatic air spray conditions were set next. Since electrostatic air spray and conventional air spray equipment were physically identical in this program, no equipment changes were required. The same procedure for establishing spray conditions was followed: setting paint characteristics, then making trial-and-error adjustments to operating conditions (including voltage, shaping air, and atomizing air) until an acceptable spray pattern was realized. Once an acceptable spray pattern was achieved, foil-covered test panels were painted and cured to assure an acceptable pattern and finish under the tentative spray conditions. This process was repeated until an acceptable pattern and finish were realized on test panels. Then spray conditions for electrostatic air spray and conventional air spray equipment were documented, fixing them at the same level for all subsequent transfer efficiency determinations in this program.

Establish Gun Portion of the Variance

The following procedure for establishing the gun portion of the interlaboratory variance was performed for each equipment type at the first laboratory. The serial number of the spray gun was recorded for each transfer efficiency determination made. Once standard spray conditions were determined as above, the order of testing was randomized to provide six replicate transfer efficiency determinations—one for each gun and each type of spray system.

The data analysis for determining the gun portion of the interlaboratory variance is described in Section 7 - Test Results and Statistical Analysis.

First Interlaboratory Test

As described above, much of the work conducted at the first laboratory involved start-up operations including: setting up the three different spray systems, paint cutting and documentation, establishing standard operating conditions for

each spray system, and conducting tests to determine the gun portion of the variance for each spray system. The first interlaboratory test consisted solely of conducting six replicate transfer efficiency tests on each of the three spray systems. No operating or maintenance variables were altered from test to test.

SUBSEQUENT INTERLABORATORY TESTS

Transfer efficiency tests at subsequent laboratories each consisted of three discrete experiments corresponding to three equipment types—electrostatic air spray, conventional air spray, and airless. Six replicate transfer efficiency determinations were conducted for each type of equipment. Subsequent test series in the interlaboratory program took 5-8 days in each laboratory. The summary of each of these test series, the problems encountered, and the test results follows.

TRANSFER EFFICIENCY TEST AT LABORATORY NO. 1 - June 3-28, 1985

The transfer efficiency tests were performed at the first laboratory to define and establish spray conditions to be utilized as a standard for subsequent testing, to calculate the gun portion of the variance, and to help determine the number of subsequent sites required to statistically prove the precision requirements of the draft transfer efficiency test method.

At the first laboratory, six replicate transfer efficiency determinations were made for each spray gun (eight each of conventional airless, electrostatic air spray, and conventional air spray). The order of the transfer efficiency determinations was determined using random number tables.

Test Set-Up

Several items were established prior to the testing including paint viscosities, the cure schedule, and the numerous operating pressures. In addition, scales, gages, and meters were calibrated to within the EPA-approved standards (see Appendix B).

Two Ford viscosity cups were calibrated against standardizing oil.

The paint cure schedule was chosen after several weight percent solid tests were performed. The cure schedule was set at 330°F for 11 minutes. It was apparent, however, that this time and temperature did not achieve complete curing. At the suggestion of the manufacturer, conditions were adjusted to 375°F for 15 minutes. Although the painted surface was apparently cured by the new schedule, paint weight continued to decline with additional curing. According to the manufacturer, this phenomenon was caused by the breakdown of a chemical crosslinking mechanism in the coating. This phenomenon was an additional concern in trying to adequately control curing of test targets.

The paint manufacturer also recommended the viscosities for airless and electrostatic air spraying using this type of paint. With the higher weight percent solids, the use of 15 seconds (No. 4 Ford cup) for electrostatic air spraying and conventional air spraying, and 30 seconds for airless spraying was advised.

The pressure gages to be used for the program were high-precision gages. They were dead-weight tested prior to TE testing.

Once the pressure gages were tested, the mass flow meter was calibrated. Several major problems existed. The airless system caused high vibrations due to the airless pump pulsations. The control panel vibrated, causing an even greater problem with the meter stabilization.

After reviewing the mass flow meter installation instructions, it was decided to place steel plates on the control panel to give the meter a more rigid base. After several trial runs, it was determined that these steel plates did dampen the vibration.

The mass flow meter was tested against the paint capture method at various flow rates. It met the accuracy requirement of \pm 0.9 percent defined in the QA/QC Plan (see Appendix B.)

Airless Testing

The airless test actually began one week after the project team's arrival on site. Using random number tables, the order in which the airless tests would be performed was derived. The order and the resultant foil numbers and transfer efficiencies are included as Table 6-1.

The airless gun test was completed in two days. The results are included in Table 6-1. The average transfer efficiency was 44.4, with a standard deviation of 2.50 across all gun types. These numbers do not have any particular value of their own; the values take on significance only when examined in conjunction with the results of the other laboratories.

Electrostatic/Conventional Air Spray Testing

This portion of the test was set up and run according to the operating parameters set up in Appendix A and recorded in the raw data sheets in Appendix E. No major problems were encountered during the testing; however, it appeared that the mass flow meter was becoming increasingly less accurate. This problem forced onsite engineers to request a change in the QA/QC requirements to + 10 grams, consistent with other acceptable mass flow measurement methods in Appendix B.

These transfer efficiency determinations were made during the last three weeks of June 1985.

Test Results

The objectives of the first test were to establish operating conditions for the eight-laboratory study, to determine the gun portion of the variance, and to perform the first part of an eight-laboratory study. These objectives were achieved.

Base Operating Conditions

As described in the preceding section, base operating conditions for all three equipment types were established during the first week of testing. They are presented in Appendix E.

TABLE 6-1. ORDER OF AIRLESS GUN TESTING

GUN	FOIL NOS.	TRANSFER EFFICIENCY
<u>616</u> 32	31-36	42.2
60838	37-42	45.7
61449	43~48	47.1
61449	49-54	46.1
60838	55-60	44.5
61632	61 - 66	40.6
60829	67-72	42.4
60429	79-84	43.1
61632	85-90	43.5
61629	91-96	44.9
60829	97-102	44.2
61629	103-108	43.8
61649	109-114	43.3
60865	115-120	44.8
61449	121-126	45.9
61632	127-132	44.1
60865	133-138	45.1
61449	139-144	47.1
61632	145-150	44.8
61449	151-156	45.3
61629	163-168	45.2
61629	169-174	44.2
61644	176-181	46.1
60838	182-187	45.1
61644	188-193	42.2
60865	194-199	44.7
61449	200-205	45.6
61629	206-210	44.2
61649	212-217	43.4
60865	218-223	42.6
000 OND	230-235	CORD CARD
61649	236-241	43.5
61644	242-247	43.4
61649	248-253	42.8
61644	254-259	43.3
61644	260-265	42.8
61644	266-267	43.9
60865	272-277	44.3
61632	278-283	43.2
60865	284-289	45.5
60838	290-295	45.0
60838	296-301	45.0
60829	302-307	42.4
60829	314-319	43.0
60838	320-325	45.1
60829	326-331	43.2
61629	332-337	44.0

Gun Portion of the Variance

The gun portion of the variance was statistically detectable and significant. Summaries of the order of gun testing, foil numbers, and the transfer efficiency results are presented in Tables 6-1, and 6-3. The variance (not standard deviation) attributable to differences between guns used during this research for the three equipment types was:

Airless 6.22 Conventional air spray . . . 0.88 Electrostatic air spray . . . 13.01

The variances for airless and conventional air spray guns were considered unexpectedly low. In the final analysis, they contributed little to the total (overall) interlaboratory variance. Electrostatic air spray variance was higher, but still accounted only for 15 percent of the total interlaboratory variance for electrostatic air spray transfer efficiency determinations.

Thus, it was concluded that the differences between guns must be accounted for even though they were not a major contributor to the total interlaboratory variance.

The determination of the gun portion of the variance is discussed in more detail in Section 7 - Statistical Analysis.

First Laboratory Test Results

After each test was completed, an outlier analysis was performed on the data (see Appendix C.)

Airless test results from the first laboratory had a mean transfer efficiency value of 44.2, with a standard deviation of 0.821. The data were tightly grouped as shown in Table 6-4. These numbers do not have any extraordinary value of their own; the values take on significance only when examined in conjunction with the results of the other laboratories. They do, however, demonstrate the capability of the draft transfer efficiency test method to produce highly repeatable data at a given facility.

The electrostatic data showed a significantly greater degree of dispersion (see Table 6-2). The reason for this trend could not be technically pinpointed nor statistically modeled; however, it was apparent that there was a constant factor influencing the testing, especially the electrostatic air spray gun tests. Test results are presented in Section 7. There was speculation onsite that the electrical supply changed during the day as heating demands, office lighting demands, and other electrical demands were made on the power supply. This speculation could not be documented.

TABLE 6-2. ORDER OF ELECTROSTATIC AIR SPRAY GUN TESTING

GUN	FOIL NOS.	TRANSFER EFFICIENCY
C1378	573-578	65.27
C1320	585-590	71.04
C1356	597-602	75.50
C1336	609-614	73.70
C1356	621-626	73.64
C1290	633-638	71.65
C1230	561-566	79.63
C1320	717-722	70.56
C1382	717-722	64.39
	729-734	62.46
C1290		
C1290	747-752	62.86
C1336	759~764	72.20
C1290	771-776	64.68
C1378	783-788	70.32
C1356	417-422	74.60
C1355	429-434	77.83
C1365	441-446	79.24
C1378	453-458	73 <i>.</i> 75
C1365	465-470	79.04
C1290	477-482	77.06
C1290	489-494	77.37
C1356	501-506	75.10
C1356	513-518	76.99
C1320	525-530	76.45
C1355	537-542	70.58
C1320	549-554	74.54
C1356	1016-1021	77.98
C1382	944-949	73.75
C1382	956-961	72.30
C1336	968-973	77.35
C1336	980-985	74.74
C1382	992-997	74.28
C1336	1004-1009	77.73
C1365	886-891	77.73 74.41
C1365	863-868	76.48
C1382	875-879 (+901)	
C1355	908-913	76.15
C1333	920-925	66.50
C1355		74.90
C1336	932-937	66.98
	795-800	70.03
C1365	807-812	7 3.89
C1365	819-824	73.71
C1368	832-837	70.76
C1378	844-849	71.68
C1378	857-862	72.11
C1320	356-361	77.61
C1355	369-374	69.71
C1355	381-386	74.10
C1320	393-398	80.30
C1320	405-410	78.83

TABLE 6-3. ORDER OF CONVENTIONAL AIR SPRAY GUN TESTING

GUN FOIL NOS. TRANSFER EFFICIENCY C1378 567-572 32.72 C1356 591-596 29.80 C1356 603-608 37.29 C1356 615-620 34.44 C1290 627-632 41.26 C1320 349-355 36.67 C1355 363-368 36.44 C1355 375-380 37.80 C1320 399-404 40.40 C1355 423-428 35.56 C1355 423-428 35.56 C1365 411-416 34.29 C1355 423-428 35.56 C1365 435-440 34.25 C1378 447-452 36.86 C1290 471-476 39.92 C1290 483-488 39.98 C1356 495-500 31.46 C1356 507-512 33.20 C1320 519-524 38.19 C1320 543-548 38.20 C1320 55-560			
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	C1356	1010-1015	29.23

TABLE 6-4. LABORATORY 1 TEST RESULTS

			
Airless			
Transfer efficiency	(%):	44.9 43.8 45.2 44.2 42.9 44.0	
Mean: Standard deviation:		44.2 0.821	
Electrostatic air spray			
Transfer efficiency	(%):	65.3 70.3 73.8 70.8 71.7 72.1	
Mean: Standard deviation:		70.7 2.89	
Conventional air spray			
Transfer efficiency	(8)	32.7 36.9 35.4 34.9 34.0 33.3	
Mean: Standard deviation:		34.5 1.53	

Electrostatic air spray equipment produced a mean transfer efficiency of 70.7 with a standard deviation of 2.89. These numbers do not have any extraordinary value of their own; the values take on significance only when examined in conjunction with the results of the other laboratories. They do, however, demonstrate the capability of the draft transfer efficiency test method to produce repeatable data at a given facility.

Conventional air spray equipment produced a mean transfer efficiency of 34.5, with a standard deviation of 1.53. Again, these numbers do not have any extraordinary value of their own; the values take on significance only when examined in conjunction with the results of the other laboratories. They do, however, demonstrate the capability of the draft transfer efficiency test method to produce highly repeatable data at a given facility.

Test Facilities

The second laboratory transfer efficiency tests were conducted in a Binks water-wash spray booth in the spray painting laboratory. The laboratory provided the spray painting laboratory, technicians, conveyor system, curing oven, and other associated test materials.

The engineering laboratory was roughly 1220 cm by 915 cm with 600 cm ceilings (about 40 ft by 30 ft, with 20 ft ceilings). The booth maintained the linear air velocity at 40.6-61.0 cm/s (80-120 ft/min), as required by the proposed laboratory selection criteria. The booth area temperature was controlled at 22.2°C (72°F) during test runs. Paint and solvent were kept in the booth area and their temperatures closely matched booth ambient temperatures. Relative humidity was controlled at 50 percent during the test.

A Mayfran Cableway overhead conveyor system equipped with a Lab-line digital timer was used in all experiments at this site. A Despatch oven was used for curing painted targets.

The laboratory was supplied with the spray gun, 5-gallon pressure tank with agitator, hoses, and 75 kV power supply. The same gun also was used to simulate conventional air spray painting by conducting transfer efficiency determinations with no voltage applied.

Transfer Efficiency Tests

Equipment set-up and instrument calibrations were completed on September 24, 1985. Transfer efficiency testing began on September 24, 1985. Six replicate transfer efficiency determinations were made for each equipment type. Airless tests were completed the first day of testing. Conventional air spray tests and electrostatic air spray tests were completed the following day. Operating conditions are presented in the raw data sheets in Appendix E.

The purpose standard transfer efficiency test method and spray conditions, as set forth in Transfer Efficiency Method Evaluation Plan, were followed for all transfer efficiency determinations. All operating conditions are presented in the raw data sheets in Appendix E. All QA/QC requirements were met, and no special problems were encountered during the experiment.

Test Results

Transfer efficiency results for these tests are presented in Table 6-5. Mean and standard deviations are also summarized in Table 6-5.

Airless test results from the second laboratory had a mean transfer efficiency value of 33.1, with a standard deviation of 1.73. The data were tightly grouped as shown in Table 6-5. These numbers do not have any extraordinary value of their own; the values take on significance only when examined in conjunction with the results of the other laboratories. They do, however, demonstrate the capability of the draft transfer efficiency test method to produce highly repeatable data at a given facility.

Electrostatic air spray equipment produced a mean transfer efficiency of 66.2 with a standard deviation of 0.95. These numbers do not have any extraordinary value of their own; the values take on significance only when examined in conjunction with the results of the other laboratories. They do, however, demonstrate the capability of the draft transfer efficiency test method to produce repeatable data at a given facility.

Conventional air spray equipment produced a mean transfer efficiency of 24.4, with a standard deviation of 0.57. Again, these numbers do not have any extraordinary value of their own; the values take on significance only when examined in conjunction with the results of the other laboratories. They do, however, demonstrate the capability of the draft transfer efficiency test method to produce highly repeatable data at a given facility.

A standard outlier test, using Nalimov's criteria, was conducted on transfer efficiency results for each spray system. One outlier was identified (Run No. 10) in the electrostatic air spray results. No reason for the outlier could be identified. The run was repeated as per the requirements of the QA/QC Plan. According to the QA/QC Plan, outlier transfer efficiency results were replaced by the results of a replacement transfer efficiency determination. Thus, outliers were not included in the final data set from each laboratory and had no effect on the results of the study.

Sequential Analysis Estimating Number of Laboratories

Results of transfer efficiency determinations from the first and second laboratory were used to estimate the number of laboratories required to estimate the method's precision satisfactorily, i.e., to ensure that the probability of the estimated variance differing from the actual variance by less than a specified amount is high. In terms of a mathematical relationship, this means:

$$Pr[\tilde{\sigma}^2 - \sigma^2 < \delta] > P$$
 (1)

TABLE 6-5. LABORATORY 2 TEST RESULTS

Airless	
Transfer efficiency (%):	35.3 34.4 33.0 31.3 33.6 30.8
Mean: Standard deviation:	33.1
Electrostatic air spray	
Transfer efficiency (%):	65.4 65.8 65.2 67.8 66.6
Mean: Standard deviation:	66.2 0.95
Conventional air spray	
Transfer efficiency (%)	24.9 25.2 24.0 24.0 23.8 24.2
Mean: Standard deviation:	24.4 0.57

where σ^2 is the square of the method precision, $\tilde{\sigma}^2$ is the estimated variance from the interlaboratory test program, and δ is the degrees of freedom. For estimation of the number of laboratories based on the results of the first two tests, $\tilde{\sigma}^2$ is the total variance between the first two laboratories. The probability (P) was specified as 80 percent by the contract sponsoring this research. Fiscal limitations allowed up to eight laboratories to be tested; if the estimated number of laboratories (based on the first two laboratories' results) exceeded eight to obtain 80 percent confidence, then only eight laboratories could be tested.

The following analysis of variance was performed for each of the three equipment types tested at the first two laboratories:

Analysis	of Variance	
First Two	Laboratories	

Source	<u>ss</u>	<u>DF</u>	<u>MS</u>
Between laboratories	ssa	1	$\mathtt{MS}_{\mathtt{a}}$
Between guns, labora- tory l	ss _b	7	мsъ
Reproducibility within guns, laboratory 1	ss _c	32	MS _C
Reproducibility, labora- tory 2	ss _d	9 49	мsа

The sum of squares (SS) divided by the number of degrees of freedom (DF) results in a value for the mean square (MS). The following equations have been derived, based on expected values of the mean squares, to determine the variance components from the test results:

$$\tilde{\tilde{c}}_{w}^{2} = \frac{32 \text{ SS}_{c} + 9 \text{ SS}_{d}}{41}$$
 (2)

$$\tilde{\sigma}_{b}^{2} = \frac{50}{1700} \left[MS_{a} + \left(\frac{1}{5} - \frac{32}{41} \right) MS_{c} - \frac{1}{5} MS_{b} - \frac{9}{41} MS_{d} \right]$$
 (3)

The desired estimate of test precision is then

$$\tilde{\tilde{\sigma}} = \sqrt{\tilde{\tilde{\sigma}} w^2 + \tilde{\tilde{\sigma}} b^2}$$
 (4)

where the $\tilde{}$ notation indicates the estimate is based on results in the first two laboratories.

The final estimates of the within- and between-laboratory variance components, based on testing at all b laboratories, were given by

$$\tilde{\sigma}_w^2 = MS_w$$
 with b(n-1) degrees of freedom
 $\tilde{\sigma}_b^2 = MS_b - MS_w / n$ with b-1 degrees of freedom
(5)

Thus the final estimate of the test precision was

$$\tilde{\sigma} = \sqrt{MS_W \left(1 - \frac{1}{n}\right) + \frac{MS}{n}b}$$
 (6)

Confidence limits may be placed on this estimate of the test precision based on the fact that the ratio of the variance estimate to the population variance, when multiplied by the number of degrees of freedom, is distributed as chi-square. This allows the variance of the estimate to be written as:

$$\operatorname{Var} (\tilde{\sigma}^{2}) = \frac{2^{\sigma} w^{4}}{b (n-1)} + \frac{2(\sigma w^{2} + n \sigma b^{2})^{2}}{n (b-1)^{2}}$$
 (7)

The initial estimate of Var $(\tilde{\sigma}^2)$ was based on the results of testing in the first two laboratories, equations (2) and (3):

$$\sigma_{\mathbf{w}} = \tilde{\sigma}_{\mathbf{w}}; \quad \sigma_{\mathbf{b}} = \tilde{\sigma}_{\mathbf{b}}$$
 (8)

Assuming that the final estimate of the precision is normally distributed with the mean of and the variance given by equation (7), then equation (1) can be used to determine the number of laboratories (b) required. This was done to determine the approximate number of laboratories that would be required to varify the efficiency of the method to a defined level. However, the actual number of laboratory test that could be conducted was governed by fiscal constraints. Table 6-6 tabulates the number of laboratories needed to validate the method for n=6, $\widetilde{\sigma}_w=1$, $\widetilde{\sigma}_b=2$.

Table 6-6. Number of laboratories (b) required to be P% sure that the estimated total variance is within K% of the true value.

Percent	relative	error	(K%)
			

Р%	20	30	40	50	60	70	80	90	100
		<u>Air</u>]	less cor	nvention	al spray sys	tems (ALC)		
90	>30	23	14	9	7	5	4	4	3
80	31	15	9	6	5	4	3	3	3 2 2 2
70	21	10	6	5	4	3	3	2	2
60	14	7	5 3	3	3	2	2	2	2
50	10	5	3	3	2	2	2	2	2
		Ī	Electro	static s	pray systems	(ALE)			
90		>30	32	21	15	11	9	7	6
80		>30	20	13	10	7	6	5	4
70	>30	23	13	9	7	5	4	4	3 3
60	33	15	9	7	5	4	3	3	3
50	22	10	7	5	4	3	3	2	2
		Air a	atomize	d conven	tional spray	syste	ms (AAC)		
90		>30	33	22	15	12	9	8	7
80		>30	21	14	10	8	6	5	
70	>30	24	14	9	7	6	5	4	5 3 3
60	>30	16	10	7	5	4	4	3	3
50	23	11	7	5	4	3	3	3	2

The results presented in Table 6-6 indicate that the ALE and AAC require approximately twice the number of laboratories as the ALC to achieve the level of confidence criteria. That criteria had an 80 percent probability of being within 2.5 transfer efficiency units of the mean. As previously indicated, however, the actual number of laboratory tests that could be conducted was governed by fiscal constraints. Thus, only the ALC program approached that criteria. For b=8, i.e., the number of tests conducted, the estimates indicate only approximately 65 percent chance of being within 50 percent of the true values. This lack of laboratory experience, naturally, reduced the scope of conclusions that can presently be made about the defined method.

Test Facilities

Tests were conducted in a Protect Aire back draw spray booth in the spray painting laboratory. The laboratory provided the spray painting laboratory, technicians, conveyor system, curing oven, and other associated test materials.

The spray painting laboratory was roughly 1220 cm by 915 cm with 600 cm ceilings (about 40 ft by 30 ft, with 20 ft ceilings). The booth was a back draw, water-wash type, which maintained the linear air velocity at 41-61 cm/s (80-120 ft/min), as required by the proposed standard transfer efficiency test method. The booth area temperature was controlled at 22.1-23.3°C (71-74°F) during test runs. Paint and solvent were kept in the booth area; paint and solvent temperatures closely matched booth ambient temperatures. Relative humidity ranged from 44 to 56 percent during the test.

A Rapistan overhead conveyor system equipped with a Century E-Plus speed control was used in all experiments at this site. A Michigan oven was used for curing painted targets.

The laboratory was supplied with a manual airless spray gun, 5-gallon pressure tank with agitator, hoses, and 75 kV power supply. The electrostatic air spray gun also was used to simulate conventional air spray painting by conducting transfer efficiency determinations with no voltage applied.

Transfer Efficiency Tests

Equipment set-up and instrument calibrations were completed on September 30, 1985. Transfer efficiency testing began on October 1, 1985. Six replicate transfer efficiency determinations were made for each equipment type. Operating conditions are detailed in Appendix E.

The proposed standard transfer efficiency test method and spray conditions, as set forth in Transfer Efficiency Method Evaluation Plan, were followed for all transfer efficiency determinations. All QA/QC requirements were met, and no special problems were encountered during the experiment.

Test Results

Transfer efficiency results for these tests are presented in Table 6-7. These transfer efficiency values are only applicable to the particular system (equipment and paint) under test at specified operating conditions. Mean and standard deviations are also summarized in Table 6-7.

TABLE 6-7. LABORATORY 3 TEST RESULTS

Airless	
Transfer efficiency (%):	49.4 47.5 44.9 48.5 46.4 50.5
Mean: Standard deviation:	47.9 2.06
Electrostatic air spray	
Transfer efficiency (%):	68.7 71.2 70.2 70.8 72.6 71.6
Mean: Standard deviation:	70.9 1.33
Conventional air spray	
Transfer efficiency (%)	39.6 39.4 39.0 39.2 39.1 38.6
Mean: Standard deviation:	39.2 0.35

A standard outlier test, using Nalimov's criteria, was conducted on transfer efficiency results for each spray system. One outlier was detected (Run No. 6) during the airless test. No reason for the outlier was determined. The run was repeated as required by the QA/QC Plan; the result was substituted for the original outlier as prescribed by the QA/QC Plan. Thus, the outlier had no effect on the results of the study.

Test Facilities

Tests were conducted in a spray painting area roughly 427 cm by 305 cm, with 305 cm ceilings (about 14 ft by 10 ft, with 10 ft ceilings). The booth was a back-draw dry filter type, which maintained the linear air velocity at 61 cm/s (120 fpm), as required by the proposed standard transfer efficiency test method. The booth area temperature was 22.2-26.6°C (72-80°F) during test runs. Paint and solvent were kept in the booth area; paint and solvent temperatures closely matched booth ambient temperatures. Relative humidity was 51-58 percent during the test.

An Econo overhead conveyor system was used in all experiments at this site. A Despatch oven was used for curing painted targets. The laboratory was supplied with a manual Wagner G-10 airless spray gun, associated hoses, high-pressure paint pump, and 015 spray tip. For electrostatic air spray transfer efficiency determinations, the laboratory was supplied with a manual spray gun, 5-gallon pressure tank with agitator, hoses, and 75 kV power supply. The electrostatic air spray gun was also used to simulate conventional air spray painting by conducting transfer efficiency determinations with no voltage applied.

Transfer Efficiency Tests

Equipment set-up and instrument calibrations were completed on October 23, 1985. Transfer efficiency testing began on October 24, 1985. Six replicate transfer efficiency determinations were made for each equipment type. Airless tests were completed the first day of testing. Electrostatic air spray and conventional air spray tests were completed the following day. Operating conditions are presented in Appendix E - Raw data.

The proposed standard transfer efficiency test method and spray conditions, as set forth in Transfer Efficiency Method Evaluation Plan, were followed for all tansfer efficiency determinations. All QA/QC requirements were met, and no special problems were encountered during the experiment.

Test Results

Transfer efficiency results for these tests are presented in Table 6-8. These transfer efficiency values are only applicable to the particular system (equipment and paint) under test at specified operating conditions. Mean and standard deviations are also summarized in Table 6-8.

TABLE 6-8. LABORATORY 4 TEST RESULTS

Airless	
Transfer efficiency (%):	39.9 42.1 38.5 36.2 35.5 36.5
Mean: Standard deviation:	38.1 2.54
Electrostatic air spray	
Transfer efficiency (%):	70.6 67.1 68.9 68.7 69.7
Mean: Standard deviation:	69.1 1.17
Conventional air spray	
Transfer efficiency (%):	34.9 35.7 35.3 35.6 34.2 36.3
Mean: Standard deviation:	35.3 0.723

A standard outlier test, using Nalimov's criteria, was conducted on transfer efficiency results for each spray system. One outlier was identified in these tests. The booth exhaust fan was not running during painting of Run No. 11. The results of this flawed test run were replaced as per the QA/QC Plan, and thus had no effect on the final analysis of the results.

Test Facilities

Tests were conducted in a Binks spray booth. The laboratory provided the spray painting area, curing oven, and assistance required to complete the transfer efficiency tests.

The spray painting area was roughly 549 cm by 1219 cm with 427 cm ceilings (about 18 ft by 40 ft, with 14 ft ceilings). The booth was a dry back filter type, which maintained the linear air velocity at 56 cm/s (110 ft/min), as required by the proposed standard transfer efficiency test method. The booth area temperature was 23-24°C (73-75°F) during test runs. Paint and solvent were kept in the booth area; paint and solvent temperatures closely matched booth ambient temperatures. Relative humidity was 65-77 percent during the test.

An overhead conveyor system was used in all experiments at this site. A Despatch oven was used for curing painted targets.

The laboratory was supplied with a manual airless spray gun, associated hoses, high-pressure paint pump, and 015 spray tip. For electrostatic transfer efficiency determinations, the laboratory was supplied with a manual spray gun, 5-gallon pressure tank with agitator, hoses, and 75 kV power supply. The electrostatic air spray gun was also used to simulate conventional air spray painting by conducting transfer efficiency determinations with no voltage applied.

Transfer Efficiency Tests

Equipment set-up and instrument calibrations were completed on November 11, 1985. Transfer efficiency testing began on November 12, 1985. Six replicate transfer efficiency determinations were made for each equipment type. Airless and electrostatic air spray tests were completed the first day of testing. Conventional air spray equipment transfer efficiency determinations were completed the following day. Operating conditions are presented in Appendix E - Raw data.

The proposed standard transfer efficiency test method and spray conditions, as set forth in Transfer Efficiency Method Evaluation Plan, were followed for all transfer efficiency determinations. All QA/QC requirements were met, and no special problems were encountered during the experiment.

Test Results

Transfer efficiency results for these tests are presented in Table 6-9. These transfer efficiency values are only applicable to the particular system (equipment and paint) under test at

TABLE 6-9. LABORATORY NO. 5 TEST RESULTS

		
Airless		
Transfer efficiency	(%):	30.1 29.9 29.5 30.5 30.1 30.7
Mean: Standard deviation:		30.1 .427
Electrostatic air spray		
Transfer efficiency	(%):	50.4 52.1 51.2 50.3 54.5 54.6
Mean: Standard deviation:		52.2 1.94
Conventional air spray		
Transfer efficiency	(%)	27.6 27.8 29.0 28.6 27.2 27.9
Mean: Standard deviation:		28.02 .664

specified operating conditions. Mean and standard deviations are also summarized in Table 6-9.

A standard outlier test, using Nalimov's criteria, was conducted on transfer efficiency results for each spray system. No outliers were identified.

Test Facilities

Tests were conducted in a DeVilbiss spray booth. The laboratory provided the spray painting area, conveyor system, curing oven, and assistance required to complete the transfer efficiency tests.

The spray painting area was roughly 427 cm by 305 cm, with 305 cm ceilings (about 14 ft by 10 ft, with 10 ft ceilings). The booth was a water wash type, which maintained the linear air velocity at 56 cm/s (110 fpm), as required by the proposed standard transfer efficiency test method. The booth area temperature was 23.9°C (75₀F) during test runs. Paint and solvent were kept in the booth area; paint and solvent temperatures closely matched booth ambient temperatures. Relative humidity was 45-70 percent during the test.

An overhead conveyor system was used in all experiments at this site. A DeVilbiss oven was used for curing painted targets. The laboratory was supplied with a manual airless spray gun, associated hoses, high-pressure paint pump, and 015 spray tip. For electrostatic air spray transfer efficiency determinations, the laboratory was supplied with a manual spray gun, 5-gallon pressure tank with agitator, hoses, and 75 kV power supply. The electrostatic air spray gun was also used to simulate conventional air spray painting by conducting transfer efficiency determinations with no voltage applied.

Transfer Efficiency Tests

Equipment set-up and instrument calibrations were completed on November 4, 1985. Transfer efficiency testing began on November 5, 1985. Six replicate transfer efficiency determinations were made for each equipment type. Airless tests were completed the first day of testing. Airless and electrostatic air spray equipment transfer efficiency determinations were completed the first day of testing. Conventional air spray transfer efficiency determinations were completed the following day. Operating conditions are presented in Appendix E - Raw data.

The proposed standard transfer efficiency test method and spray conditions, as set forth in Transfer Efficiency Method Evaluation Plan were followed for all transfer efficiency determinations. All QA/QC requirements were met, and no special problems were encountered during the experiment.

Test Results

Transfer efficiency results for these tests are presented in Table 6-10. These transfer efficiency values are only applicable to the particular system (equipment and paint) under test at specified operating conditions. Mean and standard deviations are also summarized in Table 6-10.

A standard outlier test, using Nalimov's criteria, was conducted on transfer efficiency results for each spray system. One possible outlier was identified in run No. 15 of the conventional air spray tests. In accordance with the test plan, no repeat of the run was conducted. No explanation for the possible outlier could be identified.

TABLE 6-10. LABORATORY 6 TEST RESULTS

Airless	
Transfer efficiency (%):	43.1 43.4 42.1 42.8 42.5 43.7
Mean: Standard deviation:	43.0 0.547
Electrostatic air spray	
Transfer efficiency (%):	70.4 71.3 71.8 71.3 74.6 69.2
Mean: Standard deviation:	71.4 1.80
Conventional air spray	
Transfer efficiency (%):	31.1 31.2 31.8 30.9 30.7 30.5
Mean: Standard deviation:	31.0 0.455

Test Facilities

Tests were conducted in a DeVilbiss spray booth. The laboratory provided the spray painting area, conveyor system, curing oven, and assistance required to complete the transfer efficiency tests.

The spray painting area was roughly 101.6 cm by 76.2 cm with 25.4 cm ceilings (about 40 ft by 30 ft, with 10 ft ceilings). The booth was a dry back filter type, which maintained the linear air velocity at 254-302.26 cm/s (100-119 fpm), as required by the proposed standard transfer efficiency test method. The booth area temperature was 18.3-23.9°C (65-75°F) during test runs. Paint and solvent were kept in the booth area; paint and solvent temperatures closely matched booth ambient temperatures. Relative humidity was 46-60 percent during the test.

An overhead conveyor system was used in all experiments at this site. A Gehnrich oven was used for curing painted targets.

The laboratory was supplied with a manual airless spray gun, associated hoses, high-pressure paint pump, and 015 spray tip. For electrostatic air spray transfer efficiency determinations, the laboratory was supplied with a manual spray gun, 5-gallon pressure tank with agitator, hoses, and 75 kV power supply. The electrostatic air spray gun was also used to simulate conventional air spray painting by conducting transfer efficiency determinations with no voltage applied.

In addition to supplying spray painting systems, the contractor provided paint, solvent, mass flow meter, pressure gauges, control panel, scales, weight percent solids equipment, viscosity cups, 60 test targets, foil, and other miscellaneous test equipment. An engineer and technician were present during all transfer efficiency determinations at Laboratory 7.

Transfer Efficiency Tests

Equipment set-up and instrument calibrations were completed on December 17, 1985. Transfer efficiency testing began on December 18, 1985. Six replicate transfer efficiency determinations were made for each equipment type. Airless tests were completed the first day of testing. Electrostatic air spraying and conventional air spraying tests were completed the following day. Operating conditions are presented in Appendix E - Raw Data.

The proposed standard transfer efficiency test method and spray conditions, as set forth in Transfer Efficiency Manual Evaluation Plan were followed for all transfer

efficiency determinations. All QA/QC requirements were met, and no special problems were encountered during the experiment.

Test Results

Transfer efficiency results for these tests are presented in Table 6-11. These transfer efficiency values are only applicable to the particular system (equipment and paint) under test at specified operating conditions. Mean and standard deviations are also summarized in Table 6-11.

A standard outlier test, using Nalimov's criteria, was conducted on transfer efficiency results for each spray system. No outliers were identified.

TABLE 6-11. LABORATORY 7 TEST RESULTS

Airless	
Transfer efficiency (%):	48.8 46.5 48.7 47.7 48.2 44.2
Mean:	47.4
Standard deviation:	1.76
Electrostatic air spray	
Transfer efficiency (%):	66.3 69.9 68.0 72.0 68.7 69.1
Mean:	69.0
Standard deviation:	1.91
Conventional air spray	
Transfer efficiency (%):	39.7 38.3 37.4 38.5 39.9 38.6
Mean:	38.7
Standard deviation:	0.903

Test Facilities

Experiments were conducted in a DeVilbiss dry filter booth in the engineering laboratory. Laboratory No. 8 provided the spray painting laboratory, technicians, conveyor system, curing oven, and other associated test materials.

The engineering laboratory was roughly 2300 cm by 1100 cm with 600 cm ceilings (about 75 ft by 36 ft with 20 ft ceilings). The booth was a back-draw dry filter type, which maintained the linear air velocity at 40.6-61.0 cm/s (80-120 ft/min), as required by the proposed standard transfer efficiency test method. The booth area temperature was controlled at 21.7-24.4°C (71-76°F) during test runs. Paint and solvent were kept in the booth area; paint and solvent temperatures closely matched booth ambient temperatures. Relative humidity ranged from 58 to 80 percent during the test.

A Unibuilt overhead conveyor system equipped with a Nordson Countamatic timer was used in all experiments at this site. A Grieve (Model SC 550) oven was used for curing painted targets.

The laboratory was supplied with a manual airless spray gun, associated hoses, high-pressure paint pump, and 015 spray tip. For electrostatic air spray transfer efficiency determinations, the laboratory was supplied with a manual spray gun, 5-gallon pressure tank with agitator, hoses, and a 75 kV power supply. The electrostatic air spray gun was also used to simulate conventional air spray painting by conducting transfer efficiency determinations with no voltage applied.

Transfer Efficiency Tests

Equipment set-up and instrument calibrations were completed on December 15, 1985. Transfer efficiency testing began December 16, 1985. Six replicate transfer efficiency determinations were made for each equipment type. Airless and conventional air spray tests were completed December 18, 1985. Electrostatic air spray tests were completed on the subsequent day. Operating conditions are presented in Appendix E - Raw data.

All pressure gages not previously calibrated were calibrated on a dead weight tester. Calibration curves were developed and used for pressure measurements. The mass flow meter was zeroed and calibrated, then checked against paint capture to assure its accuracy. At each flow rate a constant 1.2 percent difference was detected between the meter and paint capture methods. Thus, a calibration adjustment of 1.2 percent was applied to all mass flow measurements from the meter. Although it was not required by the test method or the QA/QC plan, a velocity profile was

developed for the test booth. The booth air velocity was well within QA/QC requirements.

The proposed standard transfer efficiency test method and spray conditions, as set forth in Transfer Efficiency Method Evaluation Plan were followed for all transfer efficiency determinations. All QA/QC requirements were met, and no special problems were encountered during the experiment.

Test Results

Transfer efficiency results for these tests are presented in Table 6-12. These transfer efficiency values are only applicable to the particular system (equipment and paint) under test at specified operating conditions. Mean and standard deviations are also summarized in Table 6-12.

TABLE 6-12. LABORATORY 8 TEST RESULTS

Airless Transfer efficiency (%): 46.0 44.6 45.7 44.8 44.8 46.0 45.3 Mean: Standard deviation: 0.652 Electrostatic air spray Transfer efficiency (%): 87.6 88.1 82.6 84.0 86.6 88.7 86.3 Standard deviation: 2.44 Conventional air spray Transfer efficiency (%): 25.9 25.6 25.4 25.3 25.0 25.9

Mean:

Standard deviation:

25.5

0.354

SECTION 7

TEST RESULTS AND STATISTICAL ANALYSIS

TEST RESULTS

The results of the interlaboratory testing of the transfer efficiency test method at eight field laboratories are presented in Tables 7-1, 7-2, and 7-3 for airless, conventional air spray and electrostatic spray equipment respectively. A summary of the statistical results for all test sites and equipment types is presented in Table 7-4.

STATISTICAL ANALYSIS

Introduction

The following statistical analysis is based on three assumptions. First, it is assumed that laboratories were selected randomly from the sample frame. This assumption cannot be tested, since there is no definitive list of members of the sample frame available. Second, it must be assumed that measurements were unbiased and made independently. Finally, it is necessary to assume that the within-laboratory variances are the same from laboratory to laboratory. There is certainly evidence that this assumption does not hold for test results for two equipment types. One possible alternative is to eliminate laboratories whose variances differ significantly from the others. is to proceed while noting this anomaly. The statistical analysis has been performed using all laboratories for each equipment type. A special discussion is devoted to this assumption on page 65.

TABLE 7-1. TRANSFER EFFICIENCY RESULTS, AIRLESS (% Transfer efficiency)

LABORATORY:	# 1	# 2	# 3	# 4	# 5	# 6	# 7	#8
RUN NO. 1:	44.9	35.3	49.4	39.9	30.1	43.1	48.8	46.0
RUN NO. 2:	43.8	34.4	47.5	42.1	29.9	43.4	46.5	44.6
RUN NO. 3:	45.2	32.9	44.9	38.5	29.5	42.1	48.7	45.7
RUN NO. 4:	44.2	31.3	48.5	36.2	30.5	42.8	47.7	44.8
RUN NO. 5:	42.9	33.6	46.4	35.5	30.1	42.5	48.2	44.8
RUN NO. 6:	44.0	30.8	50.5	36.5	30.7	43.7	44.2	46.0
MEAN STAND. DEV.		33.1 1.73	47.9 2.06	38.1 2.54	30.1 0.427	43.0 0.547	47.4 1.76	45.3 0.652
SUMMARY								
Within-lab	variance:	2.30		Standard	deviation:	1.53		
Between-lab (without gu		4 2.93						
Between-lab (including		e): 43.81						
Total varia (without gu		4 5.23		Standard	deviation:	6.72		
Total variation		e): 46.11		Standard	deviation:	6.79		

TABLE 7-2. TRANSFER EFFICIENCY RESULTS, CONVENTIONAL AIR SPRAY (% Transfer efficiency)

LABORATORY:	# 1	# 2	# 3	# 4	# 5	# 6	# 7	# 8
RUN NO. 1:	32.7	24.9	39.6	34.9	27.6	31.1	39.7	25.9
RUN NO. 2:	36.9	25.2	39.4	35.7	27.8	31.2	38.3	25.5
RUN NO 3:	35.4	24.0	39.0	35.3	29.0	31.8	33.4	25.4
RUN NO. 4:	34.9	24.0	39.2	35.6	28.6	30.9	38.5	25.3
RUN NO. 5:	34.0	23.8	39.1	34.2	27.2	30.7	39.9	25.0
RUN NO. 6:	33.3	24.2	38.6	36.3	27.9	30.5	38.6	25.9
MEAN:	34.5	24.4	33.2	35.3	28.02	31.0	38.7	ጎድ ድ
LITTERIA •	J 4 .J	27.7	23.2	33.3	20.02	31.0	30.7	25.5
STAND. DEV.:	1.53	0.565	0.345	0.723	0.664	0.455	0.903	0.354

SUMMARY

Within-lab variance: 1.22 Standard deviation: 1.10

Between-lab variance

(without gun variance): 25.41

Between-lab variance

(including gun variance): 31.63

Total variance

(without gun variance): 26.63 Standard deviation: 5.16

Total variance

(including gun variance): 32.84 Standard deviation: 5.73

TABLE 7-3. TRANSFER EFFICIENCY RESULTS, ELECTROSTATIC AIR SPRAY (% Transfer efficiency)

									= ========
LABORATOR	Y:	# 1	# 2	# 3	# 4	# 5	#_6	# 7	# 8
RUN NO.	1:	65.3	65.4	68.7	70.6	50.4	70.4	66.3	87.6
RUN NO.	2:	70.3	65.8	71.2	67.1	52.1	71.3	69.9	88.1
RUN NO.	3:	73.8	65.2	70.2	68.9	51.2	71.8	68.0	82.6
RUN NO.	4:	70.8	67.8	70.8	68.7	50.3	71.3	72.0	84.0
RUN NO.	5:	71.7	66.6	72.6	69.4	54.5	74.6	68.7	86.6
RUN NO.	6:	72.1	66.2	71.6	69.7	54.6	69.2	69.1	88.7
ME	AN:	70.7	66.2	70.9	69.1	52.2	71.4	69.0	86.3
STAND. DE	۷.:	2.89	0.95	1.33	1.17	1.94	1.80	1.91	2.44
SUMMARY									
Within-lab variance:		3.63		Standard	deviation:	1.905			
Between-lab variance (without gun variance):			79.44						
Between-lab variance (including gun variance):			: 85.03						
Total variance (without gun variance):			83.07		Standard	deviation:	8.70		

(including gun variance): 88.66 Standard deviation: 9.42

Total variance

TABLE 7-4. TRANSFER EFFICIENCY RESULTS

	AIRLESS		ELECTROSTATIC		CONVENTIONAL		
	VARIANCE	STD. DEV.	VARIANCE	STD. DEV.	VARIANCE	STD. DEV.	
WITHIN-LAB	1.22	1.1	3.63	1.905	2.3	1.5165	
BETWEEN-LAB	26.41		72.02		42.92		
GUN	6.22		13.01		0.88		
TOTAL	33.85	5.82	88.66	9.42	46.1	6.79	

Laboratory, Gun, and Within-laboratory Variance Components

For each equipment type, eight laboratories were used and six runs were made for each laboratory. An attempt was made to estimate the "between-laboratory" portion of variance and the "within-laboratory" portion, assuming, of course, a homogeneous within-laboratory variance. In addition, in a single laboratory experiment, the between-gun portion of variance was computed.

With the eight laboratory experiments, a one-way random effects model was assumed, with random laboratories. In other words, it is assumed that the transfer efficiency result is produced from a random effect due to the laboratory and a random effect representing the random "within-laboratory" effect. This model assumption is made simply because there are two components of variation in light of the way the experiment was constructed. This one-way random effects model then assumes that if we call y_{ii} the jth transfer efficiency measurement by the jth laboratory,

$$y_{ij} = \mu + \tau_i + \varepsilon_{ij}$$

where τ_i is a random component contributed because of the *i*th laboratory, and ϵ_{ij} is the "within laboratory" error. The reader can view the τ_i and ϵ_{ij} as having distributions, each having a population mean of zero and some variance. The variances will be called σ_{ij}^2 and σ_{ij}^2 for within laboratory and between laboratory respectively. Thus, there are two variances that require estimation from the data.

A standard analysis of variance procedure is used to estimate these variances and thus the standard deviations. Following elementary procedures in many statistics texts including Ott (1984) and Walpole and Myers (1985), the estimates of these "variance components" come by doing the analysis of variance of the total variation in the data. The sample variance for the two sources of variation is viewed in the experiment as

- MS_L (mean square between laboratories, the sample variance between laboratory means)
- MS_w (mean square within laboratories, the sample variance within laboratories)

Now the estimates of the two variances σ_w^2 and σ_L^2 are obtained from these two mean squares. Elementary manipulation leads to estimates given by

$$\hat{\sigma}_W^2 = MS_W$$

$$\hat{\sigma}_L^2 = \frac{MS_L - MS_W}{n}$$

where n is the number of runs taken in each laboratory. The "notation signifies that the quantity is an estimate. The main objective of determining the estimates of σ_l^2 and σ_w^2 is to ascertain a total variance or standard deviation of the method of measuring transfer efficiency. This total variance is made up of the sum of the "components of total variance," the latter being σ_l^2 and σ_w^2 . The total variance is featured as the standard deviation of a single observation of transfer efficiency taken at a random laboratory. The percentage of the total variance attributed to laboratory and within laboratory is reported. In addition, the coefficient of variation is given, the latter being the precision or "total standard deviation" expressed as a percent of the mean transfer efficiency.

The computation of the estimated variance components was made through the use of the Statistical Analysis System (SAS) PROC VAR COMP. The total variance, of course, is computed as the sum of the two components. In addition, the coefficient of variation is given. The coefficient of variation is defined as

$$C.V. = \left(\frac{\hat{\sigma}_T}{\bar{y}}\right) \times 100$$

and expressed in percentage units. Its purpose is merely to be able to express this standard deviation in a unitless way. The fact that it is expressed as a percent has absolutely nothing to do with the fact that transfer efficiency is expressed as a percent. The purpose of the coefficient of variation is to account for the fact that the precision of the measurement of transfer efficiency may very well depend on the average size of the transfer efficiency. The C.V. is intended as a method of "expressing precision as a function of the size of the measurement."

What is the interpretation of the Total Standard Deviation?

As was suggested earlier, the total standard deviation is a measure of the precision of the transfer efficiency method with a random laboratory. It should be emphasized that the quantity computed is only an estimate. However, if the true standard deviation were known, then it could be said that roughly 95% of transfer efficiency measurements would deviate from the mean by $\pm 2\sigma_7$. Based on the computations made, the bounds

mean
$$\pm 2\hat{\sigma}_T$$

represent estimates of bounds that cover 95% of the transfer efficiency measurements. But it cannot categorically be stated that $\pm 2\hat{\sigma}_{\tau}$ covers 95% of transfer efficiency measurements simply because values depend on a finite number of data points.

Airless

The average transfer efficiency for the airless equipment is 41.1167 transfer efficiency units.

- $\dot{\sigma}_{w}^{2}$ (within-laboratory component of variance) = 2.300
- $\hat{\sigma}_{i}^{2}$ (between-laboratory component of variance) = 43.8116
- $\dot{\sigma}_c^2$ (gun component of variance) = 0.8777
- σ_{ℓ}^{2*} (between-laboratory variance, minus qun variance) = 42.9339

The gun portion of the between-laboratory variance is 2.01%.

- σ_7^2 (total variance) = 46.116.
- 95.01% of this variance is laboratory variance.
 - σ_T^2 (minus gun variance) = 45.2339
 - σ_{7} (total standard deviation) = 6.7906 transfer efficiency units

Thus the standard deviation in transfer efficiency at a random laboratory is 6.7906 transfer efficiency units, which is 16.52% of the mean transfer efficiency of the experiment. As indicated earlier, the most important statistic is σ_{τ} , the estimated total standard deviation. An estimate or an approximation of bounds on transfer efficiency measurements is given by $\pm 1.28 \sigma_{\tau} = \pm 9.1$ transfer units. The purpose of the coefficient of variation was indicated earlier.

Thus, if the true standard deviation was known (we have developed an estimate), 80 percent of all transfer efficiency measurements at qualifying laboratories using the same type of spray equipment, paint, targets, and operating conditions would fall within 9.1 units of the true transfer efficiency.*

At a random laboratory, one is concerned with how close the measured transfer efficiency is to the true transfer efficiency. The results of this research indicate an 80 percent probability that the measured transfer efficiency would fall within 9.1 of the true transfer efficiency.*

^{*}Provided that our bias assumption is correct.

Conventional

Average transfer efficiency is 32 transfer efficiency units.

- $\dot{\sigma}_{w}^{2}$ (within-laboratory component of variance) = 1.2165
- $\hat{\sigma}_i^2$ (laboratory component of variance) = 31.6277
- il (qun component of variance) = 6.2190

The gun portion of the laboratory variance is 18%.

- $\hat{\sigma}_L^{2*}$ (laboratory component of variance gun variance) = 25.4087
- $\dot{\sigma}_{7}^{2}$ (total variance) = 32.8442
- 96.3% of this variance is laboratory variance.
 - ô (minus gun variance) = 26.6252
 - σ_7 (total standard deviation) = 5.731 transfer efficiency units.

Thus the standard deviation in transfer efficiency units at a random laboratory is 17.91% of the mean transfer efficiency of the experiment. It is estimated that \pm 1.282 $\mathring{\sigma}_7$ = \pm 1.282(5.731) = \pm 7.33 transfer efficiency units covers roughly 80% of the transfer efficiency readings around the mean.

Thus, if the true standard deviation was known (we have developed an estimate). 80 percent of all transfer efficiency measurements at qualifying laboratories using he same type of spray equipment, paint, targets, and operating conditions would fall within 7.3 units of the true transfer efficiency.*

At a random laboratory, one is concerned with how close the measured transfer efficiency is to the true transfer efficiency. The results of this research indicate an 80 percent probability that the measured transfer efficiency would fall within 7.3 of the true transfer efficiency.*

^{*}Provided that our bias assumption is correct.

Electrostatic

Average transfer efficiency is 69.45 transfer efficiency units.

- $\dot{\sigma}_{w}^{2}$ (within-laboratory component of variance) = 3.6302
- $\dot{\sigma}_L^2$ (laboratory component of variance) = 85.0295
- $\dot{\sigma}_c^2$ (gun component of variance) = 5.5912

The gun portion of the laboratory variance is 6.58%.

- G? (laboratory variance gun variance) is 79.4383
- σ_f^2 (total variance) = 88.6597
- 95.91% of this total variance is laboratory variance.
 - σ_{i} (minus gun variance) = 83.0685
 - $\dot{\sigma}_{7}$ (total standard deviation) = 9.4159 transfer efficiency units

Thus the standard deviation in transfer efficiency units at a random laboratory is 13.56% of the mean transfer efficiency of the experiment. As before, \pm 1.282 σ_{τ} around the mean covers roughly 80% of the transfer efficiency measurements. In this case \pm 1.282 σ_{τ} = \pm 12.03 transfer efficiency units.

Thus, if the true standard deviation was known (we have developed an estimate), 80 percent of all transfer efficiency measurements at qualifying laboratories using the same type of spray equipment, paint, targets, and operating conditions would fall within 12.0 units of the true transfer efficiency.*

At a random laboratory, one is concerned with how close the measured transfer efficiency is to the true transfer efficiency. The results of this research indicate an 80 percent probability that the measured transfer efficiency would fall within 12.0 of the true transfer efficiency.*

^{*}Provided that our bias assumption is correct.

Confidence Interval on Mean Transfer Efficiency Based on This Experiment

The previous results regarding the precision of the transfer efficiency method give an estimated standard deviation of a single measured transfer efficiency value at a random laboratory. To provide more information regarding accuracy of the method combined with precision or reproducibility, a computation was made which produced an estimate (for all three equipment types) of the transfer efficiency for the conditions of this experiment, along with a standard error of that estimate and an 80% confidence interval on the transfer efficiency.

Based on the one factor analysis of variance, random effects model, an estimate of the mean transfer efficiency for the present experiment is \bar{y} , the average TE over the entire experiment, while the standard deviation of this average is

$$\sigma_{\overline{y}_{.}} = \sqrt{\frac{\sigma_{L}^{2}}{\ell} + \frac{\sigma_{W}^{2}}{\ell n}}$$

where ℓ is the number of laboratories and n is the number of runs per laboratory. For a sketch of the proof of the above result, see Appendix D.

Now, the standard deviation of \bar{y} is estimated by $\sqrt{\frac{MS_L}{\ell n}}$, where MSL is the laboratory mean square in the experiment. (See Appendix D). This produces a t-type confidence interval on the mean transfer efficiency which is the parameter u in the experiment. Thus an 80% confidence interval on the mean transfer efficiency based on the results of this experiment (and for the conditions of this experiment, i.e., point-type, etc.) is given by

$$\overline{y}_{..} \pm t_{0.8.} \ell - 1 \sqrt{\frac{MS_L}{n\ell}}$$

These confidence intervals are as follows:

Airless - For the conditions of this experiment, the mean TE is between 37.709 and 44.493 TE units, with 80% confidence.

Conventional - For the conditions of this experiment, the mean TE is between 29.178 and 34.822 TE units, with 80% confidence.

Electrostatic - For the conditions of this experiment, the mean TE is between 64.825 and 74.084 TE units, with 80% confidence.

The purpose of this work is to get an impression of how much error might be associated with an estimate of transfer efficiency (actually, mean transfer efficiency) from an experiment such as It is obvious that if there is a "true transfer efficiency," and it was estimated from a sample mean from an experiment such as this one, a confidence interval on the "population mean transfer efficiency" is a clear way of determining the accuracy of the estimate of "true transfer efficiency." Surely, if the between-and within-laboratory variance is very large, it could be expected that the width of the confidence interval in conjunction with the standard regarding how "tight" the estimate should be is very important. For example, in the case of the conventional equipment, the width of the 80 percent confidence interval is 32.0 + 2.822. The issue then centers around whether missing by + 2.822 is good enough.

Importance of the Homogeneous Variance Assumption

As was indicated earlier, it is assumed that the withinlaboratory variance is constant from laboratory to laboratory. It is clear from the sample data that this, indeed, may not be true. It is important that this be acknowledged and that the impact of this be addressed. The fact that the within-laboratory variances differ for at least two equipment types results in the following conclusions:

- (a) Laboratories are not equal in the precision with which they measure transfer efficiency. Certainly, any future experimental effort in this area should focus on this.
- It was suggested earlier that there are alternatives (b) that could be used. The laboratories could be divided into homogeneous groups, with each group containing laboratories whose precision for measuring transfer. efficiency do not differ significantly. Thus, there would be two sets of answers, one for the high precision laboratories and one for the low precision laboratories. This is clearly undesirable. Since the intent of this work was to determine the precision of the method, it must be interpreted as one result and view the answer obtained as one result which has, in a sense, been averaged over laboratories, even though they do not perform with equal capability. Thus, it is felt that the results given are as reasonable as can be produced in the given situation.

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APPENDIX A

PROPOSED STANDARD TRANSFER EFFICIENCY
TEST METHOD

APPENDIX A

PROPOSED STANDARD

TRANSFER EFFICIENCY TEST METHOD

1.0 SCOPE

- 1.1 This method covers method verification testing at multiple laboratories to define the interlaboratory characteristics of the existing method.
- 1.2 The testing will be accomplished at a number of industrial sites under controlled defined conditions, i.e., the identical test protocol for applicable equipment will be used at different locations. The final evaluation will result in a complete characterization of the interlaboratory characteristics of the TE method.
- 1.3 A significant number of tests will be conducted to define the performance of the method for three automatic spray equipment types: air atomized conventional, air atomized electrostatic, and airless conventional.

2.0 APPLICABLE DOCUMENTS

2.1 ASTM Standards:

- D-1200 70 Viscosity of Paints, Varnishes, and Lacquers by Ford Viscosity Cup
- D-2369 81 Standard Test Method for Volatile Content of Coatings
- D-1005 51 Measurement of Dry Film Thickness of Organic Coatings
- O D-1212 79 Measurement of Wet Film Thickness of Organic Coatings
- o D-1475 60 Density of Paint Varnish, Lacquer, and Related Products
- D-3925 81 Sampling Liquid Paints and Related Pigmented Coatings

3.00 TRANSFER EFFICIENCY TEST METHOD

- 3.01 Inspect all equipment listed on Data Sheet 1 Equipment Specifications, and complete the data sheet where applicable. All equipment and materials must meet the requirements of the approved Environmental Protection Agency (EPA) quality assurance/quality control (QA/QC) plan.

 Note: Place "N/A" in all cells that do not apply.

 Ensure that the data sheet is dated and initialed by both the person recording the information and the person checking the information.

 "Type" refers to the design of a given piece of equipment.
- 3.02 Set up paint supply and mass flow measurement equipment per manufacturer's instructions.

Note:

Paint supply and mass flow measurement equipment must be grounded to avoid problems with static electricity.

- 3.03 Calibrate the mass flow measurement equipment once per week or each time that it is moved, whichever occurs more frequently.
- 3.04 Begin agitation of paint at least thirty minutes before any paint samples are taken.
- 3.05 Using a small glass jar with an airtight lid, take a paint grab sample from the paint pot.
- 3.06 Record test run number on label of jar. (Each pass of ten targets is a run.)
- 3.07 Complete Data Sheet 2 Paint Specifications.
 - Paint weight percent solids should be determined at the start of each day, at the end of each day, and any other time deemed appropriate.
- 3.08 Set up the conveyor speed measuring equipment consisting of photoelectric cells or limit switches used in conjunction with a digital timer, or timing marks on the conveyor used in conjunction with a stopwatch.
- 3.09 Cut an appropriate number of strips of 0.0037 cm (1.5 mil) thick aluminum foil to dimensions of 38.1 cm (15 in) by approximately 127cm (50in) for the testing.

- 3.10 Consecutively number each precut foil strip on the dull side using a permanent marking pen.
- 3.11 Weigh each foil strip and record the foil number and mass on Data Sheet 3 Mass of Solids Applied in the MASS OF FOIL COLUMN.

Note:

Data Sheet 3 - Mass of Solids Applied will hold the information from six runs.

- 3.12 Attach preweighed labeled foil (dull side to the target) to six targets using the method shown in Figure A-1. Attach unlabeled foil on four scavenger targets. All seams must face away from the spray equipment.
- 3.13 Mount the foil-covered targets in consecutive order from right to left (facing the booth), as shown in Figure A-2, with the foil seam on each target facing away from the spray gun.
- 3.14 Adjust all equipment operating parameters to the values desired for testing.
- 3.15 Complete Data Sheet 4 Operating Conditions and Calculations.

Note:

Cure time and temperature should be set per manufacturer's instructions.

- 3.16 Recheck operating parameters to ensure that they are correct.
- 3.17 For electrostatic spray equipment, measure the operating voltage and adjust according to manufacturer's instructions and record value on Data Sheet 4.
- 3.18 Inspect conveyor clock, stopwatch, and mass flow measurement equipment to assure that all are prepared to operate.
- 3.19 Turn on spray booth and conveyor. As the leading edge of the first scavenger target passes in front of the gun, turn on paint spray equipment and simultaneously begin mass flow measurement.
- 3.20 As the trailing edge of the last scavenger target passes in front of the gun, stop the paint spray equipment and mass flow measurement simultaneously.

- 3.21 Record the mass flow measurement on Data Sheet 4 Operating Conditions and Calculations.
- 3.22 Measure the wet film thickness on the trailing scavenger and record on Data Sheet 4.
- 3.23 Remove the painted targets from the conveyor and ensure that no paint is lost. Securely hang the coated targets on oven racks so all painted surfaces are exposed for uniform drying. Orient all targets in the same direction in the curing oven.
- 3.24 Insert racks in oven and bake at recommended schedule per Data Sheet 4. Oven door should be opened for minimum amount of time to prevent cooling.
- 3.25 Remove targets from oven and record actual cure schedule on Data Sheet 4. Cool foil to room temperature. Remove foil from each target, weigh foil and record mass on each foil and on Data Sheet 3 in the Mass of Foil Plus Paint column.
- 3.26 After weighing, store foils in appropriately labeled plastic bags, with the appropriate test run number labeled on it. The laboratory shall retain all samples until data analyses are complete. Check all data for correctness and completeness.
- 3.27 Perform the transfer efficiency calculations indicated on Data Sheet 4.
- 3.28 Repeat steps 3.05 through 3.27 for each test run.

Note:

Follow QA/QC plan for equipment calibration and for weight percent solids determinations when multiple runs are anticipated.

- 3.29 Make sure all data sheets have been checked, dated, and initialed.
- 3.30 When approximately 70 percent of the runs have been completed, an outlier analysis shall be performed. Data is to be recorded on Data Sheet 5. Repeat any outlier runs.
- 3.31 As part of Quality Assurance requirements, a QA report is to be submitted to the CENTEC Quality Assurance Officer at the end of each day.

4.0 SAFETY CONSIDERATIONS

- 4.1 According to Section 9.8 of NFPA 33, when using fixed electrostatic apparatus, the resistance of the equipment to ground should be measured at a resistance of less than 1 x 10^6 exponent Ohms.
- 4.2 If electrostatic equipment is being used, the gun-to-target distance should be at least twice the sparking distance.
 This requirement is in accordance with Section 9-7 NFPA 33.

DATA SHEET 1 - EQUIPMENT SPECIFICATIONS

	ТҮРЕ	MANUFACTURER	MODEL NUMBER	SERIAL NUMBER	RATED CAPACITY	RATED ACCURACY
LABORATORY SCALE						l
PLATFORM SCALE						
HASS PLOW HETER						
CONVEYOR TIMER						
STOPWATCH						
PAINT SUPPLY TANK						
PAINT SPRAY EQUIPMENT						
PAINT SPRAY BOOTH						
Conveyor					AIR CAP	T
PORCED DRAFT OVEN					PLUID TIP	
PAINT HEATER					NEEDLE	

A-X

DATA SHEET 2 - PAINT SPECIFICATIONS

Manufacturer Paint Type Resin Type Solvent			Manufacturer ID No. Lot No. Color								
DATE '	<u>rime</u>	RESIST- IVITY (MΩ/cm²)	VISCOSITY (sec#cup_at°C)	FULL		INGE WI (g) MPTY	r. <u>Net</u>	FULL	DISH WT. (g) EMPTY	NET	WT. %
			-	 	-	345 345			=		
				 		=			=		
-				- 2 - 2 - 3 - 1 <	-	=					
					-	 =			=		
					-						
			Children or included the control of		• •	*			=		
				· · · · · · · · · · · · · · · · · · ·		=======================================		***	=_		
				(
					·	=					

DATA SHEET 3 - MASS OF SOLIDS APPLIED

FOIL NUMBER	MASS OF POIL MASS OF POIL (g)	MASS OF PAINT (g)	FOIL NUMBER	MASS OF POIL MASS OF PLUS PAINT (g) POIL (g)	MASS OF PAINT (g)
	•	=		-	=
	-	•		-	•
	-	=		-	=
	-	-		-	=
	-	=		-	E
	-	•		-	=
RUN NUI	MBER TOTAL MASS	8	RUN N	JMBER TOTAL MASS	-
	-	#		-	E
	-	•		-	=
	-	•		-	=
	•	=		-	=
	-	=		-	
	-			-	
RUN NU	MBER TOTAL MASS	*	RUN N	UMBER TOTAL MASS	
	-	-		-	=
	-			-	•
	-	=		•	=
	-			-	=
	-	•		-	=
	-	=		•	•
RUN N	JMBER TOTAL MASS	•	RUN N	TOTAL MASS	*

TEST DATE:/	DATA COLLECTED BY:	DATA CHECKED BY:

DATA SHEET 4 - OPERATING CONDITIONS AND CALCULATIONS

FOIL NUMBERS	PRESSURE A	AT GUN (KPa) ATOM,AIR	ING RPS W/O PLUID	OPERA VOLTAGE (RV)	TEMPERATI AMBIENT	ure (°C) Fluid	BOOTH AIR RATE (cm/s)	RELATIVE HUMIDITY	GUN TO TARGET DISTANCE (cm)	CUI TIME(b)	
to											
to											-
to											
to											
to											
to											

			 		b	С	a	e •
Poil Numbers	VERTICAL COVERAGE (%)	FILM (cm) WET DRY	\mathcal{O} M rate determinati Δ (g) time(s)	on Rate (g/s)	CONVEYOR Speed (cm/s)	WEIGHT ♥ SOLIDS	NET DRY SOLIDS (g)	TRANSPER EFFICIENCY (%)
to								
to								
to								
to								
to								
to								

Data Checked by: _____ e=54.6($\frac{bxd}{axc}$)

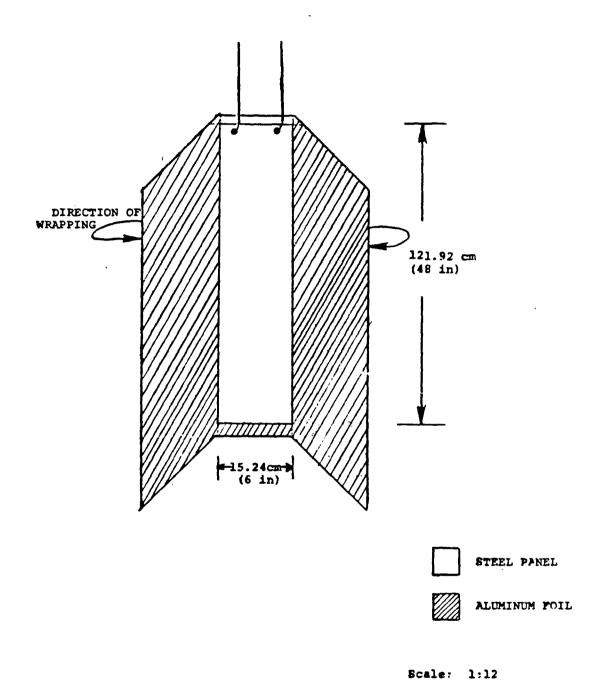


Figure 1. Foil Attachment Technique

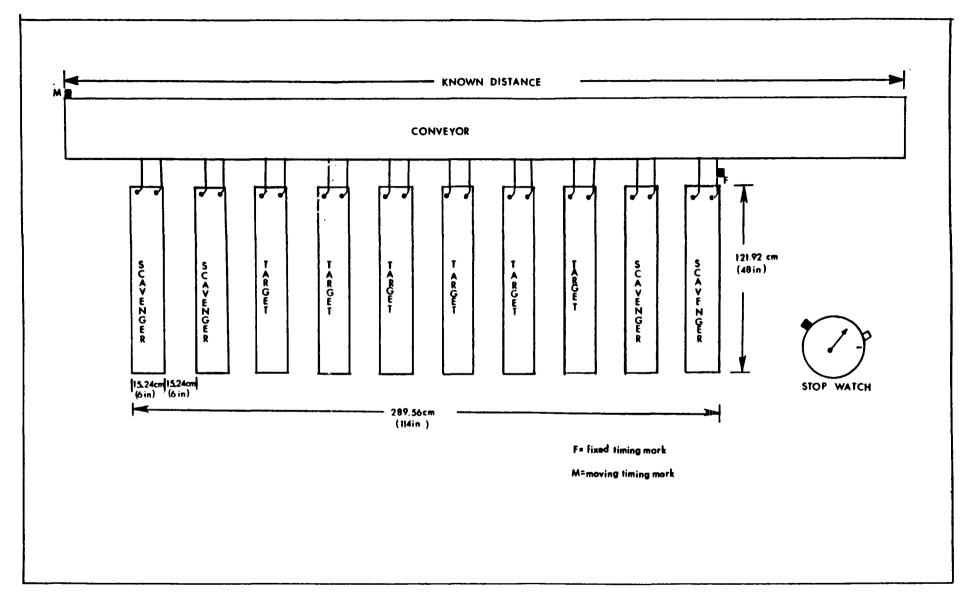


Figure 2. Target Configuration for Transfer Efficiency Determination

APPENDIX B

QUALITY ASSURANCE/QUALITY CONTROL PLAN

APPENDIX B

QUALITY ASSURANCE/QUALITY CONTROL PLAN TRANSFER EFFICIENCY METHOD VERIFICATION PROGRAM

CENTEC CORPORATION Reston, Virginia 22090

CONTRACT NO. 68-03-1952, Phase 2

AIR AND ENERGY ENGINEERING RESEARCH LABORATORY RESEARCH TRIANGLE PARK, NC 27711

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May 1985

TABLE OF CONTENTS

			Page
SECTION	1	PROJECT DESCRIPTION	.B-1
SECTION	2	PROJECT ORGANIZATION AND RESPONSIBILITY	.B-5
SECTION	3	A OBJECTIVES FOR MEASUREMENT DATA IN TERMS TERMS OF PRECISION, ACCURACY, COMPLETENESS, REPRESENTATIVENESS AND COMPARABILITY	.B-7
SECTION	4	SITE SELECTION AND SAMPLING PROCEDURES	.B-11
SECTION	5	SAMPLE CUSTODY	.B-13
SECTION	6	ANALYTICAL PROCEDURES, CALIBRATION PROCEDURES, AND FREQUENCY	.B-16
SECTION	7	DATA REDUCTION, VALIDATION, AND REPORTING	.B-18
SECTION	8	INTERNAL QUALITY CONTROL CHECKS	. B-22
SECTION	9	RESULTS OF PERFORMANCE AND SYSTEM AUDITS	.B-23
SECTION	10	PREVENTATIVE MAINTENANCE	. B-25
SECTION	11	SPECIFIC ROUTINE PROCEDURES TO ASSCESS DATA PRECISION, ACCURACY AND COMPLETENESS	.B-26
SECTION	12	CORRECTIVE ACTION	.B-28

PROJECT DESCRIPTION

INTRODUCTION

This quality assurance/quality control (QA/QC) plan assures collection of high quality data and insures consistent quality control measures for data developed under "Phase II - Method Verification Program," Contract No. 68-03-1952. Under this contract, CENTEC Corporation will be conducting tests to determine the capability of the draft standard transfer efficiency (TE) test method to precisely measure transfer efficiency.

PROJECT DESCRIPTION

This QA/QC plan is designed to ensure collection of high quality data for interlaboratory testing of the draft standard transfer efficiency (TE) test method. It encompasses the determination of the capability of the draft standard TE test method to precisely measure TE. The draft standard TE method (Appendix A) will be used for all tests in this program. The test method consists of passing a prescribed set of preweighed targets in front of spray equipment under rigidly controlled conditions in an industrial laboratory spray booth. The cured painted targets are weighed, and the original weight is subtracted from the final weight to obtain the net dry solids deposited on the targets. The net dry solids are divided by the total solids sprayed at the targets,

which is then multiplied by 100 percent to determine TE. A complete description of the draft standard TE test method is provided in Appendix A.

This objective will be accomplished by testing the method at a statistically determined number of industrial sites under controlled conditions, i.e., the same test protocol will be used at each location. Operating conditions for each spray system will be determined at the first laboratory using a trial and error approach to achieve reasonable coating thickness and finish. This technique is used by industrial finishers to set spray conditions, so test conditions are expected to simulate actual industrial practice. Once spray conditions are determined at the first laboratory, the same conditions will be specified for all subsequent laboratories in the test program. The final evaluation will result in a complete characterization of the performance of the draft standard TE test method. This evaluation includes statistical information.

TE results from previous studies using the draft standard test method have revealed information about variables which affected the TE of those particular spray systems. These variables have been shown to affect the TE of different spray systems in varying amounts; their effect is not consistent from spray system to spray system. Thus one of the major factors affecting TE, the

spray system, is being held constant in this test program. Three spray systems of different design (air atomized conventional, airless conventional, and air atomized electrostatic) will be tested at each laboratory. A new set of three spray systems (same make and model) will be used at each participating laboratory to ensure all spray equipment is in the same condition. The same coating will be used for all spray systems in this test.

Some of the variables which have been found to significantly affect TE for other spray systems include gun-to-target distance, target design, conveyor speed, linear air velocity, paint mass flow rate, atomizing air pressure, shaping air, gun condition, tip voltage, lag discharge distance, and electrode position. Test parameters which can be controlled at well-equipped painting laboratories (including gun-to-target distance, conveyor speed, paint mass flow rate, gun condition, and target design) will be specified in the test method after they are set in the first test. Special attention has been paid to ensure that difficult-to-control variables (including booth air velocity and shaping air) are consistently controlled and monitored to the extent possible. Parameters which cannot be reasonably controlled (including laboratory temperature and laboratory relative humidity) will be carefully recorded during testing. If parameters which cannot be controlled are later discovered have a significant effect on TE, enough data will be available for

assessing which variable(s) might have been the culprit. Part of the objective for this test program is to determine if uncontrollable differences between laboratories are significant.

Testing is scheduled to begin June 3, 1985, and to continue for up to eight months.

PROJECT ORGANIZATION AND RESPONSIBILITY

This project is administered through CENTEC Corporation structure, as shown in Figure B-1. Day-to-day test program activities will be managed on-site by a CENTEC Project Engineer in direct contact with CENTEC QA management personnel.

At the test site, the CENTEC engineer is responsible for implementing QA throughout the test program. The engineer conducts onsite evaluations to verify the degree of implementation, assures that appropriate QA records are kept, provides QA direction to the laboratory staff, and reports regularly to the Project Manager on the status of QA.

Dr. Ted Handel is the Quality Assurance Officer for this project. Dr. Handel functions independently from Project Management, reporting directly to the Vice President of CENTEC Applied Technology. He continuously monitors the implementation of QA and provides feedback to the CENTEC engineer onsite and to CENTEC management. Daily QA records are kept by the engineer (onsite) and submitted weekly to the Quality Assurance Officer (offsite). These records serve as resources for preparing reports and documenting adherence to QA procedures and specifications.

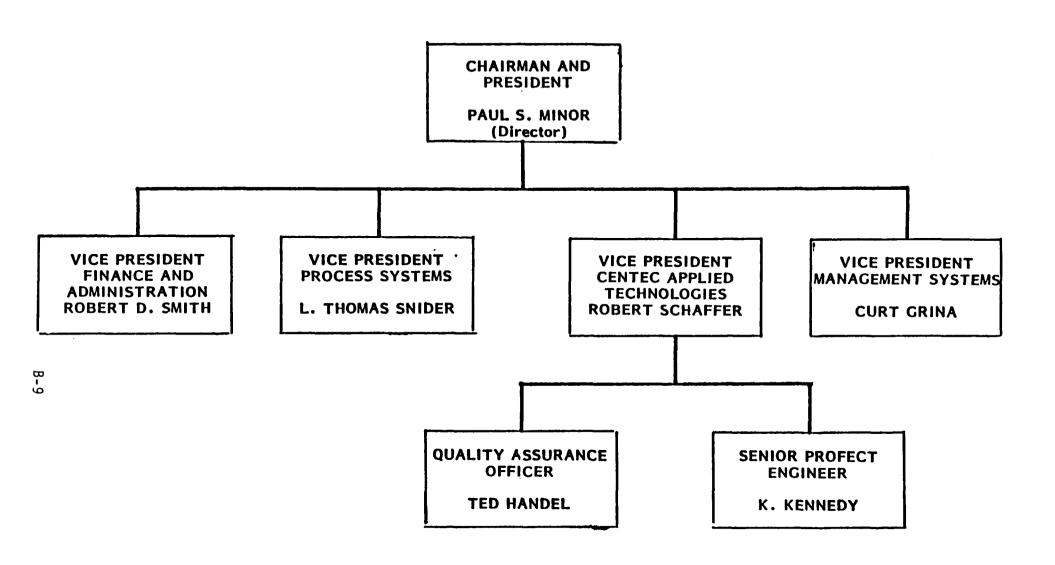


Figure B-1. Project Organization as Related to Corporate Structure

QA OBJECTIVES FOR MEASUREMENT DATA IN TERMS OF PRECISION, ACCURACY, COMPLETENESS, REPRESENTATIVENESS AND COMPARABILITY

TE test conditions will be set according to a trial and error approach at the first laboratory. Operating conditions will be set at approximate appropriate levels according to experience or manufacturer's recommendations (manufacturers' representatives will be on site for this portion of the first test), then a spray pattern will be taken. Spray conditions will be refined to correct any irregularity in the pattern, then another pattern will be taken. This procedure will be followed until the spray pattern (shape, thickness, and finish) are of reasonable industrial quality. Once an acceptable spray pattern is achieved, spray conditions will be recorded. These spray conditions will be used at all subsequent laboratories in this test program. Specified spray conditions include gun-to-target distance, fluid pressure, air pressure, shaping air, conveyor speed, voltage, pattern size, and paint viscosity. (Refer to Appendix E, Data Sheet 4.)

This technique for determining spray painting conditions is the same as industrial practice, and is therefore expected to be

highly representative of operating conditions that might have been set by industry for the systems being tested.

For each major measurement parameter, specific QA objectives for precision, accuracy, and completeness are required. These objectives are detailed in Table B-1. Not all test conditions are measured directly as listed in Table B-1, for instance, mass flow measurements may be derived from weight and time measurements and cure conditions are a combination of time and temperature.

Care must be taken to assure that all measurements are representative of the media (paint) and conditions (spray conditions) being measured. Proven techniques or methods are therefore used for all measurements.

Data quality objectives are based on accuracy and precision of each measurement, as established in Table B-1. Data integrity will be validated through a series of inspections and tests described later in this plan.

Data completeness objectives are 100 percent. This objective will be met by subjecting each data sheet to two reviews, one by a laboratory representative and one by the CENTEC Project Engineer at the test site. If a piece of data cannot be

Table B-1. Spray Painting Transfer Efficiency Precision, Accuracy and Completeness Objective

Measurement Parameter (Method)	Reference Method	Experimental Conditions	Precision (Std. Deviation)	Accuracy	Completeness
o Weight		Laboratory conditions	lab scale 0.01 g plat. scale 5 g	lab scale ±0.01 g plat. scale ±5 g	100 % 100 %
o Grounding	IEEE Std 32-1972 ANSI/IEEE Std 142-1972 ANSI C2	Laboratory conditions	-	-	100%
o Voltage	IEEE Std 4-1978	Laboratory conditions	0.05 kV	<u>+</u> 0.1 kV	100%
o Units	ASTM E 380-76/ IEEE Std 268-1976	Laboratory conditions	-		100%
o Distance-length		Laboratory conditions	0.08 cm	0.04 cm	100
o Time (stopwatch, timer)	(See ASTM 1200-70)	Laboratory conditions	0.1 s	0.2 s	100%
o Wet Film Thickness	ASTM D-1212-79	Laboratory conditions	0.265 mil	0.85 mil	1001
o Dry Pilm Thickness	ASTM D-1005-51(1079)	Laboratory conditions	2% ±0.1 mil	28	100%
o Viscosity (Ford cup)	ASTM D 1200-70(1976)		1.5 8	2 s	100\$
o Resistivity			0.1 MΩ	0.1 ΜΩ	100%
o Pressure		Laboratory conditions	<u>+</u> 1%	<u>+</u> 19	1001
o Relative Humidity	(Sling psychrometer)	Laboratory conditions	1°P	3%	1001
o Temperature (cure condi	tions)	Laboratory conditions	0.1°C	0.1°C	1001
o Linear Air Welocity (rotating vane or heated wire anenometer	ACGIH Recommended Practice, Section 9*	In accordance with NFPA 33	31	<u>+</u> 3 %	1004
o Density	ASIM D 1475-60(1980)	To be determined	±0.001 g/mL	0.002 g/mL	100%
o Wt Solids	ASTM D 2369-81	To be determined	1.50	4.78	100%
o Paint Sampling	ASIM D 3925		-		
o Condition in Container	ASTM D 3011-1		-		
o Conveyor Speed (derived	from Time and Distance)	To be determined			100
o Mass Flow Measurement (mass flow meter method)	To be determined	+0.4%	<u>+</u> 0.9 %	100%

^{*}Industrial Ventilation - A Manual of Recommended Practice, American Conference of Governmental Industrial Hygenists, 1972.

obtained, the CENTEC engineer will note the reason for failing to meet completeness objectives (i.e., power failure, broken measurement apparatus) on the data sheet. Every effort will be made to replace faulty measurement apparatus as quickly as possible. The CENTEC Quality Assurance Officer will be notified whenever completeness objectives are in jeopardy.

In the event that a test run is conducted without 100 percent completeness, the QA Project Officer will determine if the missing data are critical or if they are necessary to perform TE calculations. If the missing data are considered critical or necessary, the test run will be voided. Voided test runs will be repeated as soon as the problem is corrected. If the missing data are not integral to performing TE calculations, the QA officer will make a ruling about whether the test run should be voided and repeated, or accepted pending passing an outlier analysis.

SITE SELECTION AND SAMPLING PROCEDURES

SITE SELECTION

Previous tests have shown the importance of spray booth configuration for transfer efficiency determinations. To minimize this variable, CENTEC has developed a set of requirements that each laboratory must have in order to participate in the test program. These requirements were developed in close consultation with the spray painting transfer efficiency Steering Committee. They represent our collective best professional judgement of how to specify laboratory criteria well enough to control transfer efficiency at a satisfactory precision, but without being so stringent that only a few laboratories in the country would qualify.

First, the laboratory must be equipped with a back-draw spray booth, preferably of water wash design. Dry filter booths may be considered if filters are changed frequently to maintain air flow rates. Air velocity in the booth must be 100 fpm (plus or minus 20 fpm) in the center of the booth. Downdraft booths are not acceptable for this test program.

Participating laboratories must have an adjustable-rate overhead conveyor system capable of hanging the standardized targets as

prescribed. Participating laboratories must provide adequate laboratory balances, work areas for foil wrapping and data reduction, hangers, cleaning solvents, utilities, two know-ledgeable technicians, and security for test equipment. They must also provide a curing oven capable of accommodating EPA targets and curing them at controlled prescribed temperatures.

Given these restrictions, CENTEC began making contacts with spray equipment manufacturers, coatings companies, other interested manufacturers, paint associations, and other possible operators of spray painting laboratories. Two qualifying laboratories have already been located; they are scheduled for tests in June and July, 1985. Eight other laboratories have shown interest in participating in the test program. Information about qualifying requirements has been sent to these companies.

SAMPLING PROCEDURE

A description of the sampling procedure is provided in Appendix A, draft standard TE method. It includes:

- o A description of the test method, including references to standard methods
- o Figures illustrating specific operations
- o Description of sampling and test equipment
- o Data sheets
- Other special conditions and considerations in performing the test
- Data reduction equations

SAMPLE CUSTODY

This test program does not generate "samples" in the usual sense. This test program produces sets of data sheets and sets of painted foil targets. The data sheets and painted foil targets are considered "samples" for the purposes of this section.

The onsite CENTEC engineer will be responsible for obtaining and recording necessary information on the data sheets, and shall retain all original data generated by the test program. Procedures and forms for data sheets are presented in Appendix A. Data sheets will be stored in an orderly fashion in a Test Notebook during and after the test. The Test Notebook remains in CENTEC custody from its hand delivery to the test site, through the performance of all tests, and shall be hand carried back to CENTEC's corporate offices in Reston, Virginia. In addition to the Test Notebook, CENTEC engineers will maintain a comprehensive Log Book for special notes and observations during the test program.

Painted foils will be stored by the participating laboratory in sealed plastic bags labeled to indicate the test date, site, equipment type tested, and foil indentification numbers. Foils

will be stored by the participating laboratory until all data analysis is complete. Labels may be hand written in indelible ink on the plastic storage bags.

Field tracking reports will be kept daily, and submitted weekly to the CENTEC Quality Assurance Officer (see Table B-2). The CENTEC engineer and laboratory technician will check and sign all data sheets and tracking forms. The laboratory will retain all weighed foils, as described in the draft test method, until the data analysis is complete. Paint grab samples and target storage bag identification numbers will be recorded on sample custody sheets. CENTEC will retain all original data sheets.

Contract No. EPA 68-0	Contract No. EPA 68-03-1952								
FELD TRACKING REPORT									
Laboratory Location									
Field Sample Code Foil Number	Brief Description*	Date	Time(s)	Sampler					
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and the second of the second o									
			Nº S						
		-							
10.00 to 10.									
			<u>-</u>						
		1							
									

^{*}AAC, AAE, ALC

Table B2. Sample of field tracking report form

ANALYTICAL PROCEDURES, CALIBRATION PROCEDURES, AND FREQUENCY

ANALYTICAL PROCEDURES

Analytical procedures for determining transfer efficiency are discussed in the draft standard TE test method, Appendix A. The draft standard TE test method is not a traditional laboratory procedure; it is performed at industrial spray painting facilities using almost entirely equipment that is readily available on site. The QA/QC plan makes certain accuracy and precision requirements for instrumentation to measure test parameters, but does not specify make or model for instrumentation. Therefore, CENTEC cannot provide detailed operating and/or calibration instructions for each piece of instrumentation at every laboratory. The party responsible for conducting the TE test (in this case CENTEC) must ensure that equipment and instrumentation meet the requirements of Table B-1. The responsible party must also ensure that participating personnel follow manufacturers' instructions regarding equipment calibration, frequency, and use. If calibration or operating instructions are unavailable, CENTEC will attempt to locate instructions from the manufacturer or supplier. If unsuccessful, the engineer will report the problem to the QA Officer for resolution.

CALIBRATION PROCEDURES AND FREQUENCY

Participating laboratories will be provided with pre-calibrated test equipment for determining test pressure, linear air velocity, relative humidity. These instruments will be calibrated before and after each test series, and as deemed appropriate by either the CENTEC engineer (onsite) or the CENTEC QA Officer (offsite).

Complete manufacturer's instructions for calibration of other test equipment (including test equipment such as the mass flow meter supplied by CENTEC to participants) shall be followed for all other equipment.

DATA REDUCTION, VALIDATION, AND REPORTING

GENERAL

Data will be collected at the test laboratory under the guidance of a CENTEC engineer. The data will be collected and documented according to the requirements of the draft standard TE test method. Equations for reducing the data are also contained in the draft standard TE test method.

DATA REDUCTION, VALIDATION, AND REPORTING

Figure B-2 shows the responsible parties for each data validation and reduction step. Data reduction will be performed using*:

TE = (Weight of cured painted foil - Weight of clean foil)(100%)(Total spraying distance)
(Paint weight fraction solids)(Total solids sprayed)(Effective target width)

which simplifies to:

TE = 15,833 (Weight of cured painted foil-Weight of clean foil)
(Paint weight percent solids)(Total solids sprayed)
for the prescribed target configuration.

Any data generated by test runs with known discrepancies in performance (i.e., a smudged test panel, or a test run at different conditions than specified) will be labeled as suspect for later evaluation. Duplicate data for all suspect runs will be obtained whenever resources permit.

^{*}SI Units

CENTEC ENGINEER ON-SITE

CENTEC PROJECT MANAGER

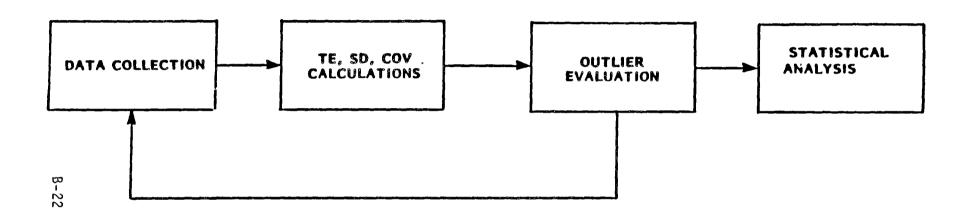


Figure B-2. Data Validation Resposibilities

For each experimental design, the reduced data will be subjected to a series of tests using Nalimov's criteria to evaluate outliers. This evaluation will be performed onsite when a test series is complete, but before taking down the spray equipment. Outliers will be replaced by duplicate runs as resources permit. The CENTEC field engineer will report any questions or problems to the Quality Assurance Officer on a daily basis.

CONSIDERATION OF OUTLIERS

Outliers will be searched for both within the data of each laboratory and among the results of the many laboratories.

Nalimov's test for outliers will be utilized. Each suspect data point within a set of data generated at a single laboratory will be tested against the mean of that data set according to Nalimov's Factor*:

$$R = \frac{|x^* - x|^2}{s} \sqrt{\frac{n}{(n-1)}}$$

where x^* is the suspect value, s is the standard deviation, \bar{x} is the mean of the set, and n is the number of observations in the set. Outliers are classified as possible, probable, or definite according to whether the value of R exceeds its 95 percent, 99 percent or 99.9 percent confidence limit respectively.

Possible outliers will be retained unless a defect in the experiment can be identified. Probable outliers will be identified and replaced with a repeated run whenever possible. Definite outliers will be rejected in every case and an experimental explanation sought.

These considerations will govern the handling of outliers among the various participating laboratories. The mean of all observations for each gun type will be tested against the mean value obtained by all laboratories, and the Nalimov criteria applied.

SECTION 8

INTERNAL QUALITY CONTROL CHECKS AND AUDITS

Internal quality control checks are incorporated into the experimental design and draft standard TE test method. These checks include a battery of six replicates for each type of spray equipment to be tested. Replicates will be examined for outliers as described in Section 8.

The use of blanks, spiked samples, and similar controls is not appropriate for this test program. Due to the nature of conducting transfer efficiency tests, these options are not practical. Since there are no reagents or calibration standards directly applicable to TE determinations, these are ruled out as well.

SECTION 9

RESULTS OF PERFORMANCE AND SYSTEM AUDITS

The performance of the TE tests will be monitored constantly as described in draft standard TE test method.

In addition, performance and system audits will be performed by the Quality Assurance Officer or by his designated representative. This designation is intended to eliminate any question of conflict of interest in the performance of audits.

After the spray painting system is operational, performance audits will be conducted to assure continued acceptable precision during testing. It is the nature of the experimental design for this program that TE results cannot be tested for outliers until a test series is complete. To minimize the likelihood of obtaining poor TE results prior to outlier analyses, internal audits are required twice daily for each major measurement contributing to TE:

- o Net solids on target, q
- o Conveyor speed, cm/s
- o Paint weight fraction solids
- o Paint mass flow rate, g/s
- o Effective target width, cm
- o Target spacing, cm

These measurements are subject to the precision, accuracy, and completeness criteria in Table B-1. They will be examined for precision and accuracy at the beginning and completion of each test series. Instrumentation such as the mass flow meter will be calibrated and checked against paint capture on a twice daily basis. Periodic audits also may be conducted during the test day as deemed appropriate by either the laboratory technician or CENTEC engineer on site. Performance audit requirements are detailed in Table B-1 and in the draft standard TE test method.

SECTION 10

PREVENTATIVE MAINTENANCE

preventative maintenance practices in the program are those recommended by the manufacturer to the spray equipment user. These practices include keeping the spray equipment and spray area clean, handling equipment carefully to avoid damage, and using appropriate equipment for the given job. These general practices must be observed to prevent inadvertent deterioration of spray equipment condition and to minimize downtime.

In addition to these preventative maintenance practices, extra electrodes and air caps should be kept on hand. Ample supplies for performing TE tests should be available to avert shortages. These include foil, paint, solvent, and other supplies outlined in the test method.

SECTION 11

SPECIFIC ROUTINE PROCEDURES TO ASSESS DATA PRECISION, ACCURACY AND COMPLETENESS

The precision and accuracy of each component the total measurement system will be documented at the beginning and end of each test series. (Refer to Table B-1.) Problems identified by the performance audit will be corrected before continuing with the test program.

Accuracy is calculated based on comparison to a reference. Pressure gages are calibrated against a laboratory-standard gage. Voltage readings obtained with the experimental equipment are calibrated against the laboratory standard, etc. Test instrumentation is adjusted until accuracy criteria in Table B-1 are met, where accuracy is calculated as:

Precision is measured as the standard deviation of a series of measurements, thereby determining the repeatability of the measurement. Standard deviation is calculated as:

$$S = \sqrt{\frac{\sum_{i=1}^{n} (x_i - \bar{x})^2}{n-1}}$$

where x is the mean of the series of measurements, x is the value obtained in each measurement, and n is the number of observations making up the series.

Determination of the overall precision of the test method is the objective of the interlaboratory test program. The completeness objective for all readings and data points is 100 percent. The method of testing for outliers presented in Section 8 during the test series, and the fact that outliers will be replaced by duplicates, will insure that completeness objectives are meet.

Completeness requirements are audited continuously and automatically by the dual check-off procedures required on each data
sheet in the draft standard TE test method.

SECTION 12

CORRECTIVE ACTION

Performance audits are required twice daily for each measurement contributing to TE. Should any measurement not meet the precision or accuracy requirements laid out in Table B-1, corrective action <u>must</u> be taken. Corrective action includes recalibration, repair, or replacement of the measurement system in question. The CENTEC engineer on site is responsible for initiating the appropriate corrective action, with concurrence from the participating required in writing in the next QA report to management.

Corrective action may also be taken to replace data identified as erroneous by the required data outlier analysis. The CENTEC Project Manager is responsible for initiating corrective action to replace outlier data.

Other corrective action may be taken at the request of onsite CENTEC or laboratory personnel whenever suspect or undocumented conditions occur. The CENTEC engineer is responsible for all such corrective actions.

APPENDIX C

DETECTION OF OUTLIERS BY MEANS OF NALIMOV'S TEST

CONSIDERATION OF OUTLIERS

Outliers were searched for, both within the data of each laboratory and among the results of the eight laboratories. Nalimov's test for outliers was utilized (see below). Each suspect data point within a set of data generated at a single laboratory was tested against the mean of that data set according to Nalimov's Factor:

$$R = \left[\begin{array}{c|c} x & -\overline{x} \end{array} \right]^2 \sqrt{\frac{n}{n-1}}$$

where x is the suspect value, s is the standard deviation, \overline{x} is the mean of the set, and n is the number of observations in the set. Outliers were classified as possible, probable, or definite according to whether the value of R exceeded its 95 percent, 99 percent, or 99.9 percent confidence limit, respectively.

Possible outliers were retained unless a defect in the experiment was identified. Probable outliers were identified and replaced with a repeated run whenever possible. Definite outliers were rejected in every case and an experimental explanation sought.

Similar consideration governed the handling of outliers among the various participating laboratories. The mean of all observations for each gun type was tested against the mean value obtained by all laboratories, and the Nalimov criteria applied.

APPENDIX D STATISTICAL ANALYSIS ADDENDUM

Appendix D

The random effects model is given by

$$y_{ij} = \mu + \tau_i + \varepsilon_{ij}$$

$$i = 1, 2, \dots, \ell$$

$$j = 1, 2, \dots, n$$

where τ_i is the effect of the *i*th lab and ϵ_{ij} is the *j*th random disturbance within each laboratory. The average \overline{y}_{ii} is given by

$$\bar{y}_{..} = \sum_{l} \sum_{j} y_{ij} / \ell n$$

$$= \sum_{l} \sum_{i} (\mu + \tau_{l} + \varepsilon_{ij}) / \ell n$$

$$= \ell n \mu + n \sum_{l} \tau_{l} + \sum \sum \varepsilon_{ij} / \ell n$$

Now, $Var(\tau_i) = \sigma_i^2$ and $Var(\varepsilon_{ij}) = \sigma_w^2$. If one takes the variance of the right hand side of the above, one obtains, after simplification

$$Var(\overline{y}_{L}) = \frac{\sigma_{L}^{2}}{\ell} + \frac{\sigma_{W}^{2}}{n\ell}$$

and thus

$$\sigma_{\overline{y}_{..}} = \sqrt{\frac{\sigma_L^2}{\ell} + \frac{\sigma_W^2}{n\ell}}$$

Now, an estimator of $\sigma_{\nu_{-}}^2$ is given by $MS_t/n\ell$. This is easily verified since standard methods reveal that

$$E(MS_L) = \sigma_W^2 + n\sigma_L^2$$

thus $MS_L/n\ell$ is an unbiased estimator of $\frac{\sigma_W^2}{n\ell} + \frac{\sigma_\ell^2}{\ell}$.

APPENDIX E

OPERATING CONDITIONS AND RAW DATA SUMMARY

LABORATORY 1

DATA SHEET 4 - OPERATING CONDITIONS AND CALCULATION	DATA	SHEET	4 -	OPERATING	CONDITTIONS	AND	CALCULATIONS
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T- 100	FOIL NUMBERS	PRESSURE AT (Rota I.PLUID	ring r W/O		VOLTAG	OPERA: B (RV)		r. (HΩ)	Temperatu Ambient	-	nid oc)	BOOTH A		RELATIVE HUMIDITY	GUN TO TA DISTANCE	RGET (cm)		ure Temp (^o c)
Trial Bunk	70012	1825	N/A	NIA	NI	4	NIF	}	NL	A	24.85	as	<u>ه</u> ور	100±20	Bm	76°10	2.5.4c		15mi	1916 (375F)
trial Run 61632	13 to 18	1825									26°C					/	1.			
61632	19027	1825									26°C					./*				
60838	వ ్ణం 30	1800									الم م					•				
61449											26.8°C					507k				
61449	30eo4)		V			/	•					\downarrow	/				→		1	
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	FOIL NUMBERS	VERTICAL COVERAGE (%)	PILM (cm				HASS PI AL (g)	LON RATI		rminat ime (=)	ION RATE (g	/s)		/EYOR D (cm/s)		IGHT \ OLIDS	NET DRY SOLIDS (g)	TRANS EFFICIE	FER NCY (%)
61632	701Z	. 3 _. 3	0.6r	us L	/A	N	/A	163.	1 14	4:4	11.32		(41	£ } /m/q)	5	8%				
61632	1300	30		_				171.	7 14	4,4	11.92	<u>-</u>			_5	8/0				
61632			06n	علد				162.5	s 1	4.0	11.6	1			5	8%				
60838	25 ^{to} 30	70	0.6 m	N				176.	6 1	3.8	12.80	2			5	80%			·	
61449	31 to 35																			
61449 61449	360041				$\sqrt{}$			L						/			· · · · · · · · · · · · · · · · · · ·			

Data Collected by:

Data Checked by: $M = 54.68 \left(\frac{b \times d}{a \times c}\right)$ or e=15.833 / d

or
$$e=15,833 \left(\frac{d}{cxf}\right)$$

6/11/85

DATA SH	eet 4	•	OPERATING	CONDITIONS	AND	CALCULATIONS
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							DATA	SHE	et 4	- OPE	ERAT	ING CO	NDITIONS	AND CAL	CULATIONS	<u> </u>			
	FOIL Numbers	PRESSURE AS	T GUN	(KPa) M,AIR	WI.E	ROTAT 'LUID	ING F	PS FLUID	VOLT	OPERJ NGE (kv)	TING RESI	s т. (нП)	Temperat Ambient	ure (°C) Pluid	BOOTH AIR RATE (cm/s)	HUHIDITY		TIME(B)	re Temp (^o c)
60838	320 325	′ /	1	//A	1	/19	NI	,	N		N	/A		26°C	100+1/n	70%	Con lion	Mi	3T
60829	26 331	1890											aar	26°C	pottle	640/0	25.4 (10m)	12n	375
	332 33												30°C	26°C	100t/m	640%	25.4m	15m	Z:15
	to																		
	to																		
	to		,							,		V							
氏 1 4				- N			Icro		n ren	f	·				Ъ	c	đ	<u> </u>	e •

4				///\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\								
	Poil Numbers	VERTICAL COVERAGE (%)	PHH (cm) WET DRY	Floure Inst. (g)	uid mass fi Pinal (g)	LOW PLATE DI Δ (g)	ETERMINATIO TIME(#)	N RATE (g/s)	CONVEYOR SPEED (Cm/s)	Weight \ Solids	NET DRY SOLIDS (g)	TRANSFER EFFICIENCY (%)
60838	to 32,0325	22%	.8rul	593d	NA	141.5	14.25	, 9,93g/s (595.8gh	40 Ft/n	45.10	23.13	45.1
	to 326 <i>3</i> 31	2 101	.7 nil	4749/		1125	14,3	7.86 9/s (472 9/m	40ff/n	43,33	17,55	43.2
61629	to 332 337	200/0	· Gmil	560		133.7	14.3	9, 289/5 560.9da	40 f1/m	44.01	21.26	41.0
l	to								40 H/M			
	to								40 ft/m			
	to				V				40+1/m			

Data Collected by:

Data Checked by: $*e=54.68 \left(\frac{b \times d}{a \times c}\right)$ or $e=15,833 \left(\frac{d}{c \times f}\right)$

6/11/85

DATA	SHEET	4	-	OPERATING	CONDITIONS	AND	CALCULATIONS
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				·	DAIA .	JIIDE.		OFER	VIII		NDITIONS	AND	CAL	COLVIIC	NS -	*	,				7
	Poil Numbers	PRESSURE AT FLUID			TATING RPS ID W/O FI			PERATI		. (MΩ)	Temperatu Ambient	ure (° Plu	-	BOOTH A RATE (CE		relative Humidity	gun to ta distance	RGET (cm)		re Temp (^o c	
60865	34 281	1810	MA	NA	MA		NA		NA	١.	2200	760	<u>C</u>	1004	18	72%	yon		15n	375	1
60838	29029B	1810									rs.c	26	عر	POUF:	1/1	72%	10 in	-	15m	375	
60828	296 307	1910				_					22°C	ale	<u>°C</u>	100 4	1/1	72%	10 in		15h	375	
408.29							· · · · · · · · · · · · · · · · · · ·		·		22°C	20	9	100F1	a	72%	10ù		159	375	
60829	to 308 <i>3</i> 13	1890									22°C	26	00	100.11	4	72%	10 in		15m	375	
68829	314 319	1890		14			\		•	7	28°C	H	\mathcal{C}	100F	1/m	72%	10in		15h	315	}
ង ! ហ					MISS	adir	<u> </u>	f				.		ь		C	đ			•	_
	Poil Numbers	VERTICAL COVERAGE (9	PILM (TET)		F JUN PL INIT. (g)		ASS FLO L (g)	rate Δ (g)		minat Me(#)	ION RATE (ç	g/a)		VEYOR D (cm/s)		icht \ Olids	NET DRY SOLIDS (TRANSI EFFICIEI		
0865	254 257	20%	· Com	P	Many	M	N I	44.1	1 1	4.4				f/n	57	,4	23.4	19	45.	5	
60838	2 9 0 296	20%	.62	nil	594		_/	42.3		4.3	597	7/5	40	Fla	57	4.	23.0	5	44	.8	
10838	296 30/	82º/	1.7m	il	593		/	141.9		14.3	9.9d 595.	38 38	40	4/n	5	7.4	23.0	26	45.	0	
1,0829	30L 30)	a o°lo	,9n	Ji.	471			12.9	19	13			401	4n	5	7.4	17.30	0	42	.4	14
७०४२१	308 30	20%	161	nl	474		/	12.8	14	4,3	9149	1/5	40f	In	57	0.4	17.5	8	43.	5	P
60819	34319	210/0	1.6 m	ا_ب	474	V		113.	0 19	1.3	7.99	5		FILM		,40	17.5		43	~	
	Data Ćo	llected b	y: AP	3									Data	Checke	d b	y:	_ *e=54	4.68	3/bxd	1	

Data Checked by: $*e=54.68 \left(\frac{b \times d}{a \times c}\right)$ or $e=15,833 \left(\frac{d}{c \times f}\right)$

Ar flow Role Atomizing Air (SCFH) Pressure (PS)

DATA	SHEET	4	_	OPERATING	CONDITIONS	AND	CALCULATIONS
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	FOIL NUMBERS	Pressure at	T GUN (KPa) ATOM,AIR		ING RPS M/O PLUID	OPERI VOLTAGE (RV)		TEMPERAT AMBIENT	and (oc)	BOOTH AIR RATE (cm/s)	RELATIVE HUMIDITY	GUN TO TARGET DISTANCE (cm)	CU TIME (B)	_ '	
C1378	5 67 7	7 psi	23 psi	390	46	NA	N/A	71:SF	25.3 C	100 Fpr	59%	:18 in	15m	475F	~
(1326	504 504	10 psi	21 ps1	300	46			71.0F	2540	100 fpm		10in	15n	4755	
61356	5 60 5	10.5ps	23.5 ps	300	46			71. SF	254(10086	57%	10 in	150	475F	<u></u>
C1336	6 to 6	10 psi	20.5pss	305	46			715F	2540	1005 pm	597.	10.n	15m	475F	1
L 1356	6 to 6	11 ps/	22.5031	300	46			71.5F	25 YC	1005pm	58%	10 in	15 m	475 F	-
C1290	to 3	10 05	71051	300	46	4		73 F	25.56	100 tpm	55%	10.0	15.1	4751	

E (f			ь	C	đ	e 4	_
3.	Foil Numbers	VERTICAL COVERAGE (%)	FILM (cm) WET DRY		uid hass e pinal (g)		eterminati(time(s)	on rate (g/s)	CONVEYOR SPEED (cm/s)	WEIGHT \ SOLIDS	NET DRY SOLIDS (g)	TRANSFER EFFICIENCY (%)	
61378	5 to 5	18	0.3mils	353	N/A	1665	2845	5.86	10 16 mj.	47.2	17.07	32.72	6.14
1320	5 5 5.55	16	0.6 mil	376		175.7	78.55	6.15		472	21.42	39.09	6.45
61356	5 to 3	ا ح	0.3mels	351		166.5	28.6	5.82		47.2	17.19	29.80	6.10
(1336	2 tog	19	0.6ml			1858	28.7	6.47		47.2	21.51	37.6.1	ľ
C13.56	0	21.5	0.4 ml	365		173.9	28.6	6.08		47.2	18.64	34.44	6.37
C 1290	6 to 3 7 2	14	O.4 mil	399	V	190.2	286	6.65		47.7	24.47	41.26	6.18

Data Collected by: MDE

Data Checked by: $\star e=54.68 \left(\frac{b \times d}{a \times c}\right)$

Dote___

or $e=15,833\left(\frac{d}{cxf}\right)$

Hower Wound (con)

				(PETH)	DATA SHE	ET 4	- OPE	RATI	NG CO	NDITIONS	AND CAL	CULATIONS				- — — —	-
S	Foil Numbers	PRESSURE AS			MO RPS W/O FEUID	Volta	OPERA Ge (kv)		st . (ΜΩ)	Temperat Ambient	ure (°C) Fluid	BOOTH AIR RATE (cm/s)		GUN TO TARGET DISTANCE (cm)	CU TIME (D)	re Temp (°c)	
Jummy 1320	3500343	10 951	15.5 _{ps}	290	36	N	/A	4	A	72F	25.4C	100 SPM	58%	lon	15 nin	LITS°F	×
1370	35to 35	9051	ZIPSI	3∞	46					68.1F	25.2	90spm	71.5	10 m	15 M		l
1355	7/2018	9 pri	22,5ps1	795	46					68.05	25.7(90 (Pn	76.0	10 in	15 m	4751	55
C1355	3 60 3	9 ps1	22.5 px1	295	46					68.5F	25.3 C	90fph	71.0%	10in	15 m	475F	V
11370	3000	7 per	50.5 ps	300	46					18.2F	25.46	90 fpm	68.07	10 in	15 m	4757	~
(1320	3 60 4	1.0 251	21.0ps	305	45			,	V	68.ZF	25.4°C	100 form	67.0%	1011	15.	4757	L

7				Florme	k	f			b	C	4	e •	_
	Foil Numbers	VERTICAL COVERAGE (%)	FILM (cm) (WET) DRY	FIDE PL	UID MASS FI PINAL (g)	LON RATE D	ETERMINATIO TIME(s)	RATE (g/D)	CONVETOR SPEED (cm/s)	WEIGHT \ SOLIDS	NET DRY SOLIDS (g)	TRANSFER EFFICIENCY (%)	
Dunny (1320	300-	18/48:315	0.5 mus	3362	N/A	160.7	287	5.6854		_49.5		1	5.95
C1320	,5ª0,55	185/18 38	0.6 mils	340 7		155.7	28.2	5.527/5 - (33137/m		46.6	17.78	36.67	5.18
€1355	368	18.5/48	0.7 mils	3:23		160.5	28.9	5.555/5		46.6	17.76	36.44	5,81
11355	3 to 8	18	0.6mlb	3377		160.1	Z8.1	5.54915 (332,491m		466	18.37	37.8	5.80
(1340	7 60 7	18	"O.7 mels	3712		158.6	28.85	5.50g/5 (329 89/m		46.6	19.01	39.3	5.16
.1370	404	15	0.7 mils	3315	V	159.7	28.9	5.537/M (331.67/m)	1	466	19.64	40,4	5.79

Data Collected by: ME

Data Checked by: = *e=54.68 $\left(\frac{bxd}{axc}\right)$ or e=15,833 $\left(\frac{d}{cxf}\right)$

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COCCERN PROMITIONS

DATA SHEET 4 - OPERATING CONDITIONS AND CALCULATIONS

DOTH AIR

	FOIL NUMBERS	PRESSURE AT			ING RPS W/O PLUID	ľ	OPERA (RV)	ting Resist, (MΩ	TEMPERAT AMBIENT	ure (°C) Pluid	BOOTH AIR RATE (cm/s)		GUN TO TARGET DISTANCE (cm)	CU Time (b)	re Temp (°c)	
C1356	4 0 1	9 psi	22.5 X	300	46	12/1	4	ŊΆ	68.2F	25.40	100 Cbw	64.%	40 in	15m	475F	~
c 1355	3 M/S	9 851	77,04	795	45.9				69.0F	25.5 C	100 Cpm	64.70	10 in	15m	4751	V
61345	7 4 C	9 ps1	27 951	295	46				69.0F	25.5人	loofpm	60%	1010	15 m	4,751	V
C1378	4 60 17	9051	220%	300	46				69.ZF	25.5 C	100 f pm	647,	loin	15m	4757	r
(1365	4 to 4	9 psi	23ps1	z95	46				70 OF	2560	100 fpn	62%	10.2	15 m	4755	V
C1796	476	9 051	21 ps	305	46	\downarrow		V	70.5 F	2560	lootbu	60%	10 1 n	1504	475 F	レ

₩					£			Ъ	C	<u>a</u>	e *	_
	Foil Numbers	VERTICAL COVERAGE (%)	FILM (cm) WET DRY	PLUID MASS F INIT。(g) PINAL (g)		eterminati Time (0)	ON RATE (g/s)	CONVEYOR Speed (cm/s)	WEIGHT \ SOLIDS	NET DRY SOLIDS (g)	TRANSFER EFFICIENCY (%)	
c 1356	3-9 2 3	20	0.5 nds	3212 N/A	153.4	28 8	5.33 g/s	28.4 F1/m	47.5	16.36	34.29	5.58
C 1365	72 60 7	Z0.5	0.6mls	3409	1629	Z8.75	5 677/5 (340.09/m)		47.5	18.06	35.56	5.94
C1365	il to u	2 7	0.6ml	3362	160.3	28.75	5.58j/s (334.5g/m)		47.5	17.10	34.25	5.84
C1378	4 to 4	19	6.5 mily	3252	156.0	787	5.44 g/s (326.1 g/m)		47.5	17.93	36.86	5.69
(1365	4 40 4	155	" O. Jmls	3352	130	28.5	5.58315 (334.596)		47.5	17.30	34.65	5.54
C1290	to 4	13	Junit. O	3492	165.6	286	5,79		47.5	2072	39.92	6.07

Data Collected by:

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Data Checked by: $e=54.68 \left(\frac{b \times d}{a \times c}\right)$ or $e=15,833\left(\frac{d}{cxf}\right)$ PARCHA PA

DATA	SHEET	4	•	OPERATING	CONDITIONS	AND	CALCULATIONS
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	FOIL NUMBERS	Pressure A			ING RPS W/O TEUID	OPERA VOLTAGE (RV)		Temperati Ambient	ure (°C) Pluid	BOOTH AIR RATE (cm/s)	RELATIVE HUMIDITY	GUN TO TARGET DISTANCE (cm)	CUR TIME(a) T		
C1296	ع می بر 5 محمی	9051	ZI P5/	310	46	W/H	NIA	71.0 F	25,6	1105bW	61%	:10 IN	1514	475 F	/
C1356	7945 500	10 051	א _א פה צב.	300	46			71.0F	25.60	100 fpm	5870	1010	15m c	175 F	1 12
1.1356	5 to 5	10 psi	23 PSI		46			70.5F	ZS.6C	100fpm	55%	1010	1211	175E	, ··
C1320	5 to 3	9 ps1	21821	305	46			71.0F	25.60	100 f AM	54%	\ Di n	1511	1751	~
1355	100 P	7 ps1	23,75051	795	46			73.5F	25,76	1009PM	57%	loin	15,44	1751	1
c 1376	17 24 57 S	9 psi	ZIPSI	305	46			73.0F	Z58C	loofpm	70%	101h	1500	475T	V

9 .						f			ь	C	d		
	FOIL NUMBERS	VERTICAL COVERAGE (%)	EXIM (cm) WE'S DRY	PLINIT. (g)		LON RATE D \$\Delta\$ (g)	eterminati time(s)	ON RATE (g/s)	CONVEYOR SPEED (Cm/s)	WEIGHT \ SOLIDS	NET DRY SOLIDS (g)	TRANSFER EFFICIENCY (%)]
-1290	4 8 8 4 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	17.5	O.Cmls	346	N/A	164.3	28.65	5.733/s (344.19/m)	28A 4/	47.5	20.46	39.88	6.00
C 1356	1997 1997	185	0.5 mily	319		151.8	z8.5	5.369/5 (319.67/m)		47.5	15.09	31.46	5.61
c1356	5 to 5	n	0.4mls	319		150.8	Z 8 . 55	5.289/5		47.5	15.70	33,20	5.53
(1370	5 to 5	15	0.7 my	345		163.8	28.6	5.73515 (343.69(m)		47.5	19.59	38.19	6.00
C 1356	5 to 5	70	*0.6 muls	364		173.1	28.5	6.07915 (364.49/m)		47.5	17.96	33.02	6.36
<1320	5 to 5	18	6.6mV	35 L	V	169.0	78.5	5.9375°	V	47.5	20,55	38.70	6.21

Data Collected by: ME

Data Checked by: = *e=54.68 $\left(\frac{b \times d}{a \times c}\right)$ or e=15.833 / d

or $e=15,833\left(\frac{d}{cxf}\right)$

AUC Flow Rote Monison Air

6/18/85

DATA SHEET 4 - OPERATING CONDITIONS AND CALCULA	DATA	CALCULATIONS
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	FOIL NUMBERS	PRESSURE AT			ING RPS	VOLTA	OPERA GE (RV)		. (MΩ)	Temperatu Ambient		BOOTH AIR RATE (cm/s)	RELATIVE HUMIDITY	GUN TO TARGET DISTANCE (cm)	CU Time (=)		
(1320	550	9051	21 051	305	46	2	/A	W	A	73 F	25.7(100 fpm	67%	10 in	15m	4751	/
C1378	to									74.5F		100 fpm	56%	1010	15 m	475F	
	to													1011	15m	475F	-
	to													1011	15m	UTSF	
	to													10.0	15m	475 F	
	to													10.n	15 m	475F	

神 							£			b	c	đ	e *	
~ 1 0	Poil Numbers	VERTICAL COVERAGE (1)	PILM (cm) (VET DRY	PL INIT. (g)			LOW RATE DI	TIME(s)	RATE (g/s)	Conveyor Speed (cm/s)		NET DRY SOLIDS (g)	TRANSFER EFFICIENCY (%)	
(1320	5 to 60	16.5	0.5mls	356	h	A	167 6	28 6	5.93315 (355.891m)	284 FH	47.5	2 0.27	38.18	6.21
(1378	to									,				
.—	to													
	to													!
	to		÷											
	to				,								. ,, , , , ,	

Data Collected by:

Data Checked by: $\star e=54.68 \left(\frac{b \times d}{a \times c}\right)$ or $e=15,833 \left(\frac{d}{c \times f}\right)$

DAY Run No.	Qun No.	Foil No.'s	Pressur Pluid/05/	at Gun Atom, Alz/Di/	Operati Voltāge(kV)	ng (Current W.)	Temper Booth	ature ^{C)} Pluid	Booth Air Rate (cm/s)	Relative Humidity	Control Supply Air	Panel Pro Atom/ / Alyn//	Paint Pot	Air Plow (seff)) //
/	1382	705-710		21,5 _{PSI}					100415		98 p. j	46. ps,	26.8	745	
3	1290	723 - 728	10 70,	21.0gs			75°F	25.6	160FHS	54 1/0	100751	46	24.8	300	V
3	1890	735-740	10करं	21.0751			76°F	25.6	1001/6	ļ			26.8	300	
4	336	753-758	1075,	2175,					-100H15		'		21,8	300	
5	1290	765-770	11 %	2175,			774	256 ⁴	10044	590/0	95	l i			1
6	1378	777 -	. 1/	22	4	V	フック	25.8					26.8		•

AY No.	Vert.	Thick. Het Film (mile)	Meter Plow Rate	Pluid Ha Total Hass (g)	ss Flow Time (s)	Rate (gls)	Conveyor Speed (cm/s)	Wt. 0 Solide	Met Dry Solids (g)	Transfer Efficiency
/	20/48	0.5	7	1705	225	5.899/s 352.769/n	304/n	48.05	17.84	33,43
7	2/48	6.7	436glr		28.85	7.2595 435.49/n	201/n		2454	37.28
3	24/48		424 glv) <i>(</i>	29,05	7.03915	205/rs		24.95	39.04
4	21/4	0.7	431g/m	208.30	29.05	7.18 gls 430gm	20+/n	,	23.42	3,5.91
<u>\</u>	2/1		431g	2 07.4	28.9	7.17 915 43091h	20 f/m		25.26	38.79
6	24/48	7	418	201.8	24.0	4.9695 417015	201/11	A	23.37	35.41

11

Date: 6/24/85

DATA SHEET 4

Data By: OKD

Data Checked By:____

Run No.	Gun No.	Foil Wo.'s	Pressuse Pluia	,		Operatin qe(kV)	g ID A	Tempe Booth	Sature C) Fluid	Booth Rate	Air (cm/s)	Pelative Humidity	Control Supply Air/>	Panel Pre Atom. Air		Alr Flow (activi	5
7	/336	789 - 794	10 psi	20/5/		NA	- Wa	X6.5%	as.8	100	ffb,	60%	98	A,3	26.8	30U	
8	1365	801 806	1125.	24psi					a5.8°C			(01°/0		410.5	26.8	285	~
9	1365	813 818	1181	23.5 psi				71°F	2586			60%	98	46.5			V
0	いい	625 830	12ps1	22.5 psi				77%	a5.49			60%	98	46.5	26.8	290	,
11	1378	413. 838	13 751	23751				7 ° F	25.8°C			60%	100	94.5	50.8	290	~
12	1378	851	. 12	23	,			7708	25.80	- 1		60%	701	46.5	26.8	3∞	V

Pun No .	Vert. Coverage	Thick. Wet Film (mile)	Heter Plow Rate	Pluid Ma Total Mass (g)	es Flow Time (s)	Rate (gle)	Conveyor Speed (cm/s)	Wt. \ Solids	Net Dry Solide (g)	Transfer Efficiency	
7	22/98	.7	4359 LM	201.8	21.0s	7.2015 432a/m	20 s/m	48%	23.95	36.63	7.56
41	26/98		426g/5	204.7	28.9 _S	7.000/s 424 alm		48 %	19.54	30.41	7.43
9	26/18	٠Д	426918M	2055	29.05	706 pls 460 glm		48 %	20,71	32.31	7.41
10	29/98	.7	385g/m	18578	29.95	6,2915 37291m		48%	19,40	34.86	6.5%
1/	21/48	17	385 glm	186.1	ع ^{9.0} ح	4.41 g/s 385 g/m		48 %	19.71	35,96	6.72
12	148	.7	388	186.1	28.95	4.44gls 386.4glm		42%	17,47	33.3 a	676

H	

Runy No.	Gun No.	Poil No.'s	Pressure Pluid	at Gun	Operat Voltage (kV)	•	Temps Booth	c)	Booth Air Rate (cm/s)	Relative Humidity	Control Supply Air	PSI Minel Pro Atom.	Pasures Paint Pot	Air Plow (settal	'n
1/12	1315	875	10ki	231/2	NA	MA	24	255%	105 F/m	58%	119	46	368	285	
2/12	1365	892 - 897	10	23.5		Xo A	22	25.8		58%	101	46	26,8	290	1
3/12	1382	869 - 874	11	22		X/5/A	22.			58%	101	46	26.8	290	-
4/12	1355	907	10	a 3			23:52	25 k		52%	101	46	268	250	L
3/12	1572	9/9-	12.5	21.5		XI^A	24°C	26°		58%	92	46	26.8	290	سرا
6/12	1355	926-	. 10	23		XIA	a5°	26 ⁰	V	10%	93	46	268	290	4

Run No.	Vert. Coverage	Thick. Wet Film (mile)	Heter Plow Pate	Fluid Ma Total Mass (g)	es Flow Time (s)	Rate (gls)	Conveyor Speed (cm/s)	Wt. % Solide	Net Dry Solids (q)	Transfer Efficiency	
1/2	23/48	17	35/5/5	169.4	28.6	5.95 g/1 353, 389	nant/m	50%	17,10	30.50	6
1/12	25/48	.7	357	172.4	28.9	5.979/5 35079/11		D%	17.89	31.75	4
3/12	29/ /48	フ	337	162.9	29.2	5.589/S 334,7 9/		50%	18.37	34.49	} {
1/12	22/42	7	374	179.6	287	375		50%	20,59	34,87	0
5; [12		1.0	305	152,5	28.0	5.446 326.76		50 %	14.02	31,22	2
6/ 1/2	27/47	ク	381	183	28.9			57%	20.09	34,62	(

DATA SHEET 4 AAC

Date: 6/85/85

Data Checked By: MDC

Run No.	Gun No.	Poil No.ºs	Pressure Pluia		Operati Voltāga(kV)		Tempe Booth	ature C)	Booth Air Rate (cm/s)	Relative Humidity	Control Supply Air	Panel Pre Atom. Air	Paint Pot	Air Flow (activity	
7/12	1382	938-943	12	21.5	NA	NA	25	25.8	1001/8	78%	95	16	26.8	290	-
8/12	1382	950-955	12	22			26	25.8		74%	95	46	26.8	495	~
9/12	1336	962-	0	20			de	26		16%	96	46	24.8	300	~
NE	1336	974- 979	10	20.5			24	26		78%	96	460	24.8	305	V
11/12	132	986-	12	22			24	26		79%	96	46	26.8	290	-
M	1336	998-	10	20	V	1	di	26	1	78%	96	46	24.8	Log	

Run No .	Vert. Doverage	Thick. Wat Film (mile)	Heter Plow Rate	Fluid Ma Total Mass (g)	ss Plow Time (s)	Rate (gls)	Conveyor Speed (cm/s)	Wt. \ Bolide	Net Dry Solide (g)	Transfer Efficiency	
7/12	248	.6	325	156.3	28.95	323,949	n 2041s	50%	17.89	35.18	5.69
8/2	27/48	.7	326	157,2	a9.0	54295 3259/19		50 %	17.84	34.96	5.6
9/12	27/8	.7	383	184.6	a9.0	6. 3 4 gls 381,92		50%	21.08	35.06	6.6
1%		つ	382	144.5	23.95	382.38		50%	20,95	34.85	6.6
11/12	4/4/	.1	33(r	1425	29,0	560gls 336.2		50 %	18.35	34.79	5.8
12/12	28/	-7	345	185.5	28.9	6.429K		50%	21.35	35, <i>0</i> 8	6.7

Run No.	Gun No.	Foil No.'s	(PS Pressure Pluid	aE Gun Atom, Air	Operati Voltage(kV)	=	Tempa ;	ature C) Pluid	Booth Air Rate (cm/s)	Relative Humidity	Control Supply Air	Panel Pro Atom. Air	esures Paint Pot	Air Flow (actm)
1/1	1356	1010-	325	22.5	N/A	NA		25.6	100/15	76%	100	46	26.8	25
									<u>.</u>					

Run No.	Vert. Doverage	Thick. Wet Film (mile)	Heter Plow Rate	Fluid Har Total Mass (g)	Time (s)	Rate (gls)	Conveyor Speed (cm/s)	Wt. \ Bolide	Het Dry Bolide (g)	Transfer Efficiency
1//	26/ 48	.6	311	1484	38.7	5.17 Els	10.16 Cm/s	49.28	14.0	29.23
								 : 		
	<u> </u>									
	 	!								

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5.40

6/19/85

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PICFOUNDAL CONTON ACE

PICFOUNDAL CONTON

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0,5mil

0 6 mls

DATA SHEET 4 - OPERATING CONDITIONS AND CALCULATIONS

	FOIL WUMBERS	PRESSURE AT	GUN (kpa) ATOH, AIR		N/O PLUI	D VOLTA	OPERATI E (RV) R	ng Esi st. (M Ω)	temperat Ambient	ure (°C) Pluid	BOOTH AT RATE (Cm/	R RELATIVE HUMIDITY	GUN TO TARGET DISTANCE (cm)	Cure Time (b) Temp	° C)
C1378	5 to 7 3	7 psi	23,05/	300	46		MAL	250	72 F	25.ZC	100 SF	n 59%	: 10 m	15m475	FV
L1320	5 60 9	10 psi	21 psi	305	40	74 2	7 11 1	750	71.5F	25.40	100fp	m 557.	10in	15m 475	F
C1356	5 to 607	10.5 psi	23.5pg	300	46	74 1	30uA	250	71.ST	25,40	1005	n 59%	10in	15m 42	J V.
C1334	6 to 6	10 051	70.5ph	305	46		304A	250	72F.	25,5C	100£	58%	10 in	151475	F
(1356	c to b	11 ps	22.5ps	360	46	74k	29 n A	750	73 F	255C	1009	pr 58%	10.n	15m 475	F
	o to XX	10 ps 1	21.051	305	46	74K	zsuA	750	73 F	2550	10026	n 55%	1010	15m 479	F
E - 16							£			B	b	c	đ	e •	
	Poil Numbers	VERTICAL COVERAGE (%)	PILM (c WET		PLUIC IT. (g) PI		LOW RATE å (g)	Deterhinat Time (,)			NVEYOR ED (cm/s)	WEIGHT \ SOLIDS	NET DRY SOLIDS (g)	TRANSFER EFFICIENCY (, , , , (5)
(1375	5 to 5 7 8	20.5	0.61	mil 3	57 1	J/A	1696	78.55	5.94	3/2 10	0.16	47.2	34,55	65.27	6.23
C 1370	\ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \	17.5	0.6	mul 3	367		175.1	Z8.55	4		114	47.2	38.81	71.04	6.43
C1356	1 60 2	21	0.3	rul 3	52		167	28 6				47.2	34.32	75.50	
(1336	6 to 6	71	0.6	me 3	392		1865	28.7	6.5	0	7	47.2	42.70	73.70	1 22

2855

23.75

6.10

6.64

1865

174.2

111.0

Data Collected by:

Data Checked by: $*e=54.68\left(\frac{bxd}{axc}\right)$ or $e=15,833\left(\frac{d}{cxf}\right)$

46,04

6.97

47.2

47.2

47.2

AIR FOURAT Atomitur (Fe.)

6/18/85

	FOIL NUMBERS	PRESSURE AT			ING RPS	VOLTAG	OPERA!	ring Resi st. (M Ω)	Temperati Ambient	URE (°C) PLUID	BOOTH AIR RATE (cm/s)	RELATIVE HUMIDITY	GUN TO TARGET DISTANCE (cm)	CU T ime()	ire Temp (^o c)
Ł	5 to 5	9051	ZI psi	310	46	77/1	35ms	250	74 °F	25.7(100 F.D.	68%	10 in	15m	475F
18	to							,250					10 16	15/1	Y7SF
	to							750	:				10 14	150	
	to							250					1 D in	15m	475F
	to							250						15m	475 C
į	to							250					10.0	ĺΣnι	4760
							f			1	b	c .	đ	,	••
	POIL Numbers	VERTICAL COVERAGE (N) WET (Cm) DRY IN	FLUID LT. (g) PI	Mass Fi Nal (g)	LON RAT	e determinat) time(=)	ion Rate (4			eigh t \ Solid s	NET DRY SOLIDS (g)	TRANS EFPICIE	
20	3000	19	0.0	6	357	V/A	14.5	78.65	5.92 9	315 31-10	ill only 1	17.5	42.21	79,	63
78	to														
	to														
	to	·													
	to		÷												
	to					/									

or $e=15,833 \left(\frac{d}{cxf}\right)$

Date: 424/85

DATA SHEET 4

Data Checked By:

	Run No.	Gun No.	Foil Wo.'s	Progence Pluia PSI	1 / /	Operati Voltage(kV)	7 104/	Temper Booth	atuse C)	Booth Air Rate (cm/s)	Polative Humidity	Supply .		Paint P5/	Air Plow (actual)	
his run to say performed main	10	1382	711 - 716	13ps1	ZI.Spy	-30	-0-	25.60	カチ	1007 Han	52%	100	46.	26	300	
I have	16	1382	717-272	. 13ps,	21,501	75	30	75°}		100H/M		98	46	26.8	300	V
"Morsey)	2	1390	729-73	f 10 ps,	21.0 0	15	30	75'F	25,6	£108/1/19	90%	98	46	26.8	-300	~
	3a	1290	741 -746	10ps i	ZJ.opsi	74	32			18081/m	56%		46	24.8	300	
pares	3b	1290	747-152	10psi	21.0751	75.	35	769	25.60	1001/Jn	(10%)	98.	46	24.8	300	
E-18	4-		759-76A	10psi	ZI ps 1		28	76°1=		100+ 14	610%	98	465	26.8		.,
_	5	1290	<u> 771-77</u> 183-788	11 psi	2 (251	75	35	76ºF	25.6°			98	46	26.8		~

Run No.	Vert.	Thick. Wet Film (mile)	Meter Flow Rate	Pluid Ha Total Hass (g)	ss Flow Time (s)	Rate (gls)	Conveyor Speed (cm/s)	Wt. 9 Solids	Het Dry Solide (g)	Transfer Efficiency	Adjusted how
/n	20	0.7	35-3K	171.00	28.85	5,4491s	10.16cm) 20f/8	48% -	· V		6.22
15	20/	0.7	36 Zg/s		28.9	6.01915 (360.83-h		48%	38.41	70.56	6.30
Z	21/48	0.7	422,	209.4	29.0	7.05 9/s 422 g/m	wilm	44%	41.17	64.39	7.40
3a	20/42	06	424	205.4	19.0	7.09 Ugis 424.96d	201/1	48%	40.10	62.46	7.43
3/2	20/4E	0.7	423	205.3	29.1	7.05g/s 123.39	20-1/11	45%	40.19	62.86	7.40
4	25/48	 	434	209.5	29.0 29.0	7,22 J 7,15915 429.191m	20-1/100	48%	17.30	72.2	7 58
15	1/48	0.7	407	200 6	24.0	429.14 im		_ 47%	111.97	64.68	7.51

DATA SHEET 4 - OPERAT

DATA SHEET 4	-	OPERATING	CONDITIONS	AND	CALCULATIONS
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	FOIL Numbers					OPERATING GUN VOLTAGE (kV) RESIST. (MΩ)		, , , , , , , , , , , , , , , , , , , ,		BOOTH AIR RATE (cm/s)	RELATIVE HUMIDITY	GUN TO TARGET DISTANCE (cm)	Cui Time (a) 7	re Temp (°C)	
C1356	1 20 47	م م	22.5%	300	45.5	73 kV	250	68.ZF	25.56	90 ft/m	64 %	1010	15 M	4757	
C1355	479	9 851	ጄኔ <u>የ</u> ና!	300	46	74 KY 30MA	250	69.0F	25.5C	150 E/m	6070	10 in	15 m	475F	V
C 1365	578 19 77	9 psi	22 051		46	74 kV	250	19,55	2 5.5(100 C+/m	60%	Join	15m	475F	
C1378	U to 12	9 051	27. psi	300	46	TYKY	750	してつで	25.50	100 41/6	6470	1010	15	475F	e e
(1365	4 to 4 7 0	9 psi	23 ps	z95	46	74 k 35	250	71 SF	25.5°C	100 Ft/m	60%	10 in	Pan	475F-	/
C1796	7 to 82	9 181	zlps	305	46	74 3	240	71.0F	25 56	110 %	61%	10 in	150	4751	/
e '															

. 19						f			ь	С	đ	9.4	•
	Poil Numbers	VERTICAL COVERAGE (%)	FILM (cm)	PLI INIT. (g)		LOW RATE D	eterminatio Time (0)	ON RATE (g/s)	CONVEYOR SPEED (cm/s)	WEIGHT \ SOLIDS	NET DRY SOLIDS (g)	TRANSFER EFFICIENCY (%)	
C1356	4 to 4.7	기	0.5 mbs	34	N/A	153.7	28.9	5.32 515 (319.13/m)	10.16cm	47.5	3553	74.40	5.51
ر،355	7%T	21. 5	0.7 mb	340		163.8	24.9	5.67 3/5 13:10.15/m)		47.5	39.53	77.83	5.94
(136°	47.	24	o.cmis	336		160.9	78.75			47.5	39,70	79.24	5.86
C 175719.	4 to 4	19.5	0 amb	3,27		156.7	28 S	5.44315 (326,57/m)		47.5	35.88	73.75	5,6
C13/F	4 to 4	اح	0.7 mile	338		161.4	288	5.609/5 1336.39/m		47,5	39.60	79.04	5.St
CIZIO	4 to 52	17.5	0.7 muls	351	V	166.4	Z8.7	5,907/3	\bigvee	47.5	40.0°	77.06	6 08

Data Collected by:

Data Checked by: $*e=54.68 \left(\frac{bxd}{axc}\right)$ or e=15.833 / d

or $e=15,833\left(\frac{d}{cxf}\right)$

PICTOR DATA SHEET 4 - OP

DATA	SHEET	4	-	OPERATING	CONDITIONS	AND	CALCULATIONS
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	FOIL NUMBERS	Pressure A Pluid			ING RPS	OPERI VOLTAGE (RV)	TING (**)?` RESIST. (MI)	Temperati Ambient	ernid Re (oc)	BOOTH AIR RATE (cm/s)		GUN TO TARGET DISTANCE (cm)	CUR Time(D) T		İ
C1290	1 to 7	9 ps,	ZI psi	310	46	71 KV	250	71.0F	256C	100 57	60%	: 10 in	15 m	1175 F	レ
C 1356	5 to 5	10 kil	22.75ps	305	46	7412	250	71.0F	25 K	100 kg	5870	10.0	1314	475F	V
C.1356	5 to 8	10 psi	53 B2(300	46	71 KV 30M	250	70.5 F	25.66	100 FI	54%	101n	1500	47,5F	/
C1320	S to S	9 psi	کا محا	305	76	73kV	250	71.0F	25. G	100 Ft	54%	1010	1514	475F	V
21355	5 to 4	9 ps	Z3.73ps	295	46	74 × 28 m	2 750	730F	25.66	100th	70%	loin	1512	475F	~
C1370	\$ 20 \$	9 ps	الام ال	305	46	74×4-	290	73.5 F	27.00	100 54	70%	10.11	1500	475F	
20						f			9.	b	c	đ	. •		

20						f			b	c	đ		_
	Poil Numbers	VERTICAL COVERAGE (%)	WET CON)	PL INIT. (g)			eterminati Time(s)	on Rate (g/s)	CONVEYOR Speed (cm/s)	Weight \ Solids	NET DRY SOLIDS (9)	TRANSFER EFFICIENCY (%)	
L1290	4 to 4	18	0.7 mb	345	n/A	164.2	28.65	5.717B (343971m)	10.16cm/s	47.5	39.56	77.37	5.98
(1356	5 to 50 G	22	0.4mb	317		150.7	28.55	5.289/5 (316.79/m)		47.5	35.5/	75.10	5.53
C 1356	5 6 8	-22	0,6 mils	324		154.4	Z8.7	5.38315 (322.80/m)		47.5	37.06	76.99	5.63
C 1370	5 to 5	18.5	chu C.O	349		165.Z	78.6	15.78975 (346,691m		47.5	39.61	76.45	6.06
C1355	ر ده ع د مي م	24	0.6mls	363		172.8	28.6	6.047/5 (362.59/m)		47.5	38,20	70,58	6.33
(1750	G to 5	17.5	0.7 muls	355	V	168.7	28.55	5.91713 (354.571)		47.5	39.45	74.54	[6.A

Data Collected by:

Data Checked by: $e=54.68 \left(\frac{b \times d}{a \times c}\right)$ or $e=15,833 \left(\frac{d}{c \times f}\right)$

jtun No.	Gun No.	Poil No.'s	Pressure Pluid	PS;) at Gun Atom, Air	Operati Voltáge (kV)	nġ Current (.:	Temper Booth	ature ^{C)} Fluid	Booth Air Rate (cm/s)	Relative Humidity	Control Supply Air	Panel Pre Atom. Air	Paint (DS) Pot	Air Plow (scf=1)
1/1	1354	1916	. 22.5	1/	74	35	<i>20.</i> 5	256	1004/5	76%	100	16	26.8	340
											_			
										•				,

Run No.	Vert. Doverage	Thick. Wet Pilm (mile)	(a)a)	rluid Ma Total Mase (g)	es Flow	Rate (gle)	Conveyor Speed (cm/s)	Wt. 4 Solids	Net Dry Solids (g)	Transfer Efficiency
1/2			315	151.0	29.0	. 1	10.16	49.28	37.7	77.98
							-			

E-21

5.45

Date: 6/85/85

AAE

DATA SHEET 4

Data By;

Data Checked By:____

Run No.	Gun No.	Poil No.ºs	Pressur Pluid	at Gun Atom, Air	Operati Voltāge(kV)	•	Tempe:	ature C) _{Fluid}	Booth Air Rate (cm/s	Polative Humidity	Control Bupply Air	Panel Pro Atom. Air	(PS/) Paint Pot	Air Flow (scfm)	
1/12	1382	949-	12	71.5	75	35 XO) /	26	100f/s	76.4,	16	46	26.8	295	L
8/12	l	954-	12	22	74	32	250	a6°		72%	96	46	26.8	300	L
1/12	1336	968-	10	Zo	74	30	260	06°		74%	96	46	26.8	305	-
14/12	1336	a40- 985	10	a0.5	74	30	265	24		72%	96	46	24.8	3/0	,
11/12	1382	992	12	22	74	35	27	27		740%	96	46	24.7	295	1
12/12	1336	1009-	. 10	10	74	35	27	27	↓ ↓	76%	96	16	24.8	3/0	-

Rum No.	Vert. Doverage	Thick. Wet Pilm (mile)	Heter Plow Rate	Pluid He Total Mass (g)	se Flow Time (e)	Rate (gle)	Conveyor Speed (cm/s)	₩. • Bolide	Net Dry Bolids (g)	Transfer Efficiency	
7/12	26/2	1.2	375	154.4	29,0	5,40g/s 304g/M	201/5	50%	37.50	73.75	5.65
8/12	7 4 /48	.7	327	156.8	28.9	5.48915 325.51/M		51) g	34.96	72:30	5.68
9/1		.7	364	7157	21.05	383 Kala		50 %	44.44	77.35	6.70
	27/18	.60	38/	184.9	34.1	4.25 gk	w	<0.00	44,80	74:74	6.66
			339	162.3	28.8	3.64 g/s 338.8191	И	SN 7/	39,51	74.28	5.11
12/	28/40	.6	386	1411.9	29./	642915 385.49/m		C6 %	47.00	77.73	6.73

DAY Rust No.	Qun No.	Poil No.'s	PS Preseure Pluid	at Gun	Operat Voltāga(kV)	ing Current (A	Tempe Booth		Booth Air Rate (cm/s	Relative Humidity	Control Bupply Air	Pinel Pro Atom. Air	resures Paint Pot	Ale Flow (sets)	} }
1/2	1365	886-	10	23.5	74	30 xin	22	25.5	1004/1	58%	100	46	28.8	290	0
2/12	1365	443-	10	a35	74	30 -6	12	25.5		50%	100	46	268	299	~
3/12	1382	475- 879 +01	//	22	74	35,1	23	25.5		58/0	100	46	26.8	295	V
4/12	1355	90% -	10	23	74	30 16	22	25.5		60%	101	46.5.	24.9	290	~
3/2	1582	920 - 925	12.5	21.5	75	35 X/0	24	26		70%	101	96	26.8	360	-
1/1	1355	932 - 937	. 10	23	74.5	35 to	સર્ક	26	1	72%	100	460	26.8	290	$\bigg] u$

Pun Vert.	Thick. Wet Film (mils)	Heter Plow Rate	Pluid Ha Total Hase (g)	os Plow Time (e)	Rate (gle)	Conveyor Speed (cm/s)	Wt. 9 Solids	Not Dry Solids (g)	Transfer Efficiency
1/2 23/4	8 7	357	171.5	29.15	5.94 g/s 3549 7/n	201/11	50%	41.72	74.41
1/2 /4:	1.7	340	1735	29.05	5.976k		50 %	43.09	76.48
31 25/ 112 /42	. 7	333	160.8	29.0	5.51 95		50 %	39.75	76.15
1/12/4	21.0	377	180.7	28.9	6.25 g/s		50%	39.70	64.50
8/2 c1/1.	7.7	301	194.2	26.9	5.139/5 307/7/da		50 %	36.20	74.90
1/2 738/4	77	384	185D	24,0	4.389/5 362.74/1		50%	40.33	66.98

23

AAE
DATA SHEET 4

Data By: OHD

Data Checked By:____

Stun No.	Gun No.	Poil No.'s	Prossure Pluid	at Gun Atom, Air	Operati Voltage (kV)	ing Ourrent A	Temper Booth	ature ^{C)} Pluid		th Air to (cm/s)	Relative Humidity	Control Bupply Air 75	Panel Pro Atom Air PSI	Paint Pot	Alr Flow (acfm)	
7	1336	795-mD	(PSI)	P51 20	35 KV	74.0A	71.5F	35.00	10	xoup.	58%	98	9105	26.8	3∞	V
7	1 5 6 5	807 - '	11 ps 1	24psi	30/2V						600p	98			290	/
q	1365	819-	llpsi	24ps i	20 W	75 ₁	かず	26.4°C			54%				280	V
10	1378	932 83.7	12 _{psi}	27,5 ps,	30,1	741	17:5	U.9	1		59%			24.8	290	~
	138	844 849	12 psi	23 ps.	30 KV	75x104	77.5	Ur.4			410/0	98	46,5	20.8	285	V
12	13B	857-862	12/51	23751	3514	75	775	26.4	1	/	58°	98			285	V

Run No.	Were.	Thick. Mot Film (mile)	Noter Plow Rate	Fluid Ma Total Mass (g)	es flow	Rate (gls)	Conveyor Speed (cm/s)	Wt. 4 Bolide	Net Dry Bolids (g)	Transfer Efficiency	
7	26/48	,7	435	210.1	28.961	7.27gb	20f/m	48°h	41,23	70.03	7,64
8	27/18	.7	425gn	204.4	28.855	0.			47,50	73.89	7.44
9	28/46	.7	426	25.4	29.0	7.0895 4249th			47.32	73.11	7.43
Ŋ	21/40	. 7	384	185.9	29,5	6,30915 379,9014	l	,	40.80	.70.76	6.61
11	21/48	.7	387	187.	29.1	6.9595 38971			11.93	71.48	6.77
12	25/48	·7	388	187	29.0	4.045/5 386 g/m	9		42,12	72.11	6.76

E-2

Air rough Airman

DATA SHEET 4 - OPERATING CONDITIONS AND CALCULATIONS

N	FOIL MUMBERS	PRESSURE AT			ING RPS W/O PEUID		NATING GUN Y) RESIST. (MI)	Temperat Ambient	ure (°C)	BOOTH AIR RATE (cm/s)		GUN TO TARGET DISTANCE (Cm)	CU Time(a)	re Temp (^o c)	
Punmy 1320	740.8	lapsi	اجم 55ا اجم 55ا	285	36	75 kV/	N 250	69.0F	25.2C	100 Fpm	58%	:10 m	15 M	475F	V
1320	5 to 36	9 ps1	Z1 pS1	300	46	73KV	250	68.0F	257(90 fpm	7270	10 in	15m	475F	~
1355	357e0374	9051	22.Sps1	2715	46	73kV	250	68.0F	25,2(100fpm	737	10 in	15M	4758	~
17:55	p 20 3	9 psi	27 5ps	295	46	73kV 35m	750	68.0F	25.46	901pm	6970	10 in	ISM	475F	V
1320	20 to 40	9 psi	نتوک، هح	305	us	7344	750	68.5F	25,46	100 fpm	69 %	10 in -	1511	475F	1
_1320 	7 20 7	9.0 psi	21.0 p	305	45	73k	250	68.2F	25,46	100 f pm	6570	loin	154	4755	V

25						f			Ъ	C	<u>a</u> .	••	
Dumpy	FOIL NUMBERS	VERTICAL COVERAGE (%)	PILM (cm)		UID MASS I PINAL (g)		eterminati Time(0)	ON RATE (g/s)	CONVEYOR SPEED (Cm/s)	Weight \ Solids	NET DRY SOLIDS (g)	TRANSFER EFFICIENCY (%)	3/5
1320	24 5 J	16/49 = 333	0.7mls	3347	N/A				10.160mb	49.5			
1320	spec and	18/48	0.7 ml	329		1583	Z8.Z	5,617/5 (336.85/N)		46.6	38,28	77.61	5.১%
1355	360374	19/	0.7 mil	333		160.4	28.85	5.569 15 (3336519)		466	34.03	69.71	5.82
1355	3906	20/	0.7mls	336		161.9	Z885	5.613/5 (336.77/m)		46.6	36.55	74,10	5.88
.1320	3 8	18	"0.7mls	379		158.8	28.9	(3297711)		46.6	38.73	80.30	5,75
_1320	4 6 -	18	0.6	301	\downarrow	159.6	28.9	5.57715 (331.3714)	h	46.6	38.22	78.83	5.78

Data Collected by: MDE

Data Checked by: $*e=54.68 \left(\frac{b \times d}{a \times c}\right)$ or e=15.833 / d

or $e=15,833\left(\frac{d}{cxf}\right)$

Date 6/10/85
Team M.Ebrith, L.Berry, 60/8m

ALC 1

DATA SHEET 4 - OPERATING	CONDITIONS	AND	CALCULATIONS
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							ATA	SHE	et 4 ·	- OPE	ERATIN	ေလ	NDITIONS	AND CAL	CULATIONS				
June#	FOIL NUMBERS	PRESSURE AT					HG RP W/O F		VOLTAG	OPERA B (RV)	ting resiet	• (HΩ)	TEMPERATI AMBIENT	ernid (oc)	BOOTH AIR RATE (cm/s)		GUN TO TARGET DISTANCE (CM)	CU! Time(a) 1	RE Temp (^o c)
61632	34 60 36	1825	N	/A	2/	/A	N	A	7	/A	N	//	aloc	26.32	1008:10	\Te°10	25.4cm	(15m	(375F)
40838	37 *° 4Z	1400											ع ا ^و ل	26.49	(100 A/ni	06190	25.4cm	15 nun	375F
61449	43 * •48	1825			\Box									-کاد،4۰۲	i \	610/0	25.4cm		375°F
61409	49to54	1825											ar oc	24.46	100H/m	61%	con (15m	5750
60838	5500 GO	1400											21°C	26.40	(100fln)	U1º/0	25.4em (10m)	15mi	375°F
61632	61 2066	1425		,	V		<u> </u>	<u> </u>	1		1	,	a0.5℃	24.5%	(100f/m)	62%	25,30M	139	375°F
E-26							mlhe.	w	د د د د د د د د د د د د د د د د د د د	f					b	С	đ	(•
	I		1			chi	1)						CALC	dt 1					1

26				Trommeter	<u> </u>			D	C	<u> </u>	
	POIL NUMBERS	VERTICAL COVERAGE (%)	PILM (cm) WET DRY	Flow Pluid M INFF. Registing	ASS FLOW RATE DI L (g) Δ (g)	eterminati Time(0)	CALCUL RATE (9/s)	Conveyor Speed (cm/s)	Weight \ Solids	NET DRY SOLIDS (9)	TRANSFER EFFICIENCY (%)
61632	31 60 36	25%	Coils	8.83K	125.88	14.15	9.92915 (535,2)	41 ft/m	57.25	18:97	47.7
60838	37 60 42	140/0	(omils	580alm	138.2	14.25	9.73915 (58.3.901m)	41 Hm	57.25	22.38	45.7
61447	43 °° 48	16%	Comela	Not take	125.3	14.15	(533,20h)41 A/m	5 7.25	21.08	47.1
4449	49 ^{to} 54	15%	6 mile	5489/M	129.3	14.15	9.2 g/s	41 Hm	\$7.25	21.35	46.1
60839.	55060	1790	7 mus	590g/m	140.4	14.1	9.96915	41 ft/m	57.25	72.32	44.5
611,32	(100 (d)	17%	lonile	543 /	128,2	14.1	9.14915 54815/al	4/4/m	57.25	18.70	40.64
			7 11 71				· — J/M				•

Data Collected by: 3/B

Data Checked by: $*e=54.68 \left(\frac{bxd}{axc}\right)$

or $e=15,833\left(\frac{d}{c \times f}\right)$

DATA	SHEET	4	-	OPERATING	CONDITIONS	AND	CALCULATIONS
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		2222222		1							NDITIONS								1
	FOIL NUMBERS	PRESSURE AT		WI.PI	wtating r Luid W/O		VOLTAG	OPERAT		T. (MN)	Temperati Ambient	PLUID	BOOTH RATE (c		relative Humidity	GUN TO TARGET DISTANCE (cm)		ire Temp (^o c	,
60829	67°012	1865	NA	N	IA N	A	1//	†	[]	A	21.0°C	26.4	14 100	Ah (60%	25.46n (10m)	15m	275°C	
40829	73to 16	1460									21.0°C	24.9	Y 1004			Sec. 11 '	15m	375°C	
60829	792084	1.69									21.0°C		1		60%	25,40n 10cm	15m	3750	
61632	& ° 90	18a5									21.0°C	26.6	T 100A	Jan	6 h./a	25.4cm	15h	375C	
	71096	1425		Ш							2100	,a4.	59100F	+ Jain	60°/0	25.4cm	15 in	3756	ĺ
60829	97002	1860	V			1	<u> </u>				21.04	ر مالا. الا	100t	+/n	60°10	as.4cm	15m	375°C	-
E-27					Frmil	uter		f		•		1	ь	•	C	đ		••	
7	POIL NUMBERS	VERTICAL COVERAGE (%) PILM ((cm) DRY	E/12/12	LUID	HASS FI	LON RATE \$\Delta\$ (g)		rminat Time (=)			CONVEYOR PEED (cm/s)		CHT \	NET DRY SOLIDS (g)	TRANS! EFFICIE		
40829	6 7° 72	17%	Con)	44691	s		110,0	4 19	7.25	7.74	9/5/2	11ft/n	57.	25	16.53	42.	4	
60829 Revenof	75 78	17%	.bni		44391			142	3 10	4.25	10.02	ls 2	141m		.25	16.86	33.	4	\ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \
60429-	7900 84		7mi		460	5		109.	61	4.29	7.71	8/	H191/m	57	.25	16.73	43	.1	
41632	8 5:• 90	1706	I I		5400			1281	21	4.25	9,014	15/4	1Alm	57.	25	19.75	43.	.5	
	1000	140/0		,	53 lal		1 7	126.	Hi	470	8.88g	15/2	11ft In	-7	25	20.08	44	9	
61629	13) to 96	14 10	·7n	W_	- 14	21		1201	<u>' </u>	• • •	71 7 27 V		111/2	1 <i>2 /</i> :	7.2				1
61629	17°102	15°(V)	·5n	• •	46491	1	1	110.			7 22	15	1 Alm	57.		17.20	44	٦.	

Data Checked by: $e=54.68 \left(\frac{bxd}{axc}\right)$ or $e=15,833 \left(\frac{d}{cxf}\right)$ Data Collected by:

1 1 -					DATA SHE	et 4 =	• OPE	RATING CO	NDITIONS	AND C	ALCULAT:	ONS	·			
6/10/85	FOIL NUMBERS	PRESSURE AT		ROTA	TING RPS	*******	OPERA1		TEMPERAT		BOOTH RATE (AIR	RELATIVE HUHIDITY	GUN TO TARGET DISTANCE (cm)	CUITIME (•)	
1629	(03 108	1825	NA	NIA	NA	NF	1	NA	20.8°C	26.9	5°C (100	412	62%		ISM	3759
61649	to 109 114	1825		1			************		20.8°C	२७.5	000	Ha	62010	25.4cm	15m	375°C
- 1 . 1 . 7	to 115 120	1850							21°C	24.8	e (100	(/m)	60,5%		15h	3750
61449	to 126	1840		1					22°C	25.	7000	91	62%	25.41m	15 m	3750
	to 127 132	1840		1/					31°C	95.	7 100	[]m	61%	es 4en	Sir	375
	133 138		Ψ	V					31.0	25.1	0 100t	m	22%	25.4		i
- 28	 -				on rali		f				Ъ		С	đ		• •
	POIL NUMBERS	VERTICAL COVERAGE (1)	FILM (c	DRY IN	(g) FIN	MASS FLO AL (9)	% RATE & (g)	E DETERMINAT TIME(#)	ion rate (CONVEYOR PEED (cm/s		CIGHT N	NET DRY SOLIDS (g)	TRANS! EFFICIE!	
1629	to 103 108	17%	(.6 m	ls) 50	Hadm		128.8	14.15	9.10 3 (546)	915	404/1	1 5	7.25	20.53	43.	78
1649_	10 ⁴ 1 114	18%	(. 7m	(a) 5	03dn		133,	14.2	1560	1/5	ADF+IM	5	7.25	20.92	43.	3
9865	115 120	20%	(.7n	is 6	189/11		144,0	14.4	5 602	75 5 VI	40ft/m	57).40	23.26	44,	8
1999	21 126	15%	16mi	es 5	42g/4		130.	0 14.3	<u> </u>	59/a	40H/n	5	7,40	21.57	45	9
1632	127 13	15%	"(1 7m	13/2	94	1	30. a		5400	15 1	10 /1/n	5	7,40	20.73	44.	
0865	to 3313	180/0	(,7m	19 59	79g/m	/	43.	8 14.3	603.	25 c	40.A/m	5	7.40	Z3.4S	45,	/
I	Data Col	lected by	* (<u>) f/3</u>	-	, ,					Da	ta Chec	ked l	о у :	_ *e=54.6	$8\left(\frac{b \times d}{a \times c}\right)$)
													01		$33\left(\frac{d}{cx}\right)$	_/

DATA SHEET 4 - OPER	ATING CONDITIONS	AND (CALCULATIONS
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	FOIL NUMBERS	PRESSURE AT			ING RPS W/O FLUID	OPERA VOLTAGE (RV)		Temperati Ambient	ure (°C) Fluid	BOOTH AIR RATE (cm/s)	RELATIVE HUHIDITY	GUN TO TARGET DISTANCE (cm)	Cure Time(=) Temp (^o c)
1149	39°194	1830	NIA	NIA	NA	NA	NIA	20,5°C	of or	100+/5	78%	(10m)	15m 35
61632	145 60	1840						a/°C	26.2°C	100F/S	% %	25.4cm	15h 375
61449	5) 56	1840						21°C	26.2°C	100F/S	70%	85.0 CM	15m 37.5
61619	157162	1840						91°C	26.2°C	100f/s	70%	25.40m)	1Sm 375
61629	43 KB	1850					1	2100	26.28	100+15		25.40m	15m 375
6/629	169 174	1850	V		V		\bigvee	21°C	26.20	100Ft	70%	25.4m	151 375
-25				2	MSS,				•	h	c	d	••

.9				FLOW		f		•	ъ	C	, d	••
	POIL NUMBERS	VERTICAL COVERAGE (%)	PILM (cm) WET DRY	MITEC _{PL}	UID HASS F PINAL (g)	LOW RATE DI Δ (g)	eterminati Time (6)	MAID (9/8)	CONVEYOR SPEED (cm/s)	WEIGHT \ SOLIDS	NET DRY SOLIDS (g)	TRANSFER EFFICIENCY (%)
111	139 144	20%	(.7 nils)	not. Teroided	MA	130.2	14.35	9.10,15	10) HOHA)57.40	21.14	45.0
11632	14 1D	22010	(. 8 mils	545gh		130.1	14.3	9.0979/	6 Y401/1	57.40	21.06	4-4.8
19149	15/ 156	2000	(6 mile	548 g/m		131./	14,3	9.16918 550 191	(40 6/17	57.40	21.42	45.3%
61449	to 157 162	16%	(Canils	50041	_	136.1	14.3	9.52 d/s 57 N. Kla	(40F/n	57.40	ZZ.15	45.0%
41629	163 18	150%	(.7mil	55/9/2		131.6	14.3	9.20 6,15 552.16	(40+/m)	57.40	21.48	45.2%
61629	169 179	20%	(.Zajis			1375	14.3	9.26 g st 555, 94	40 F/m	57.40	21.13	44.2%

Data Collected by

Data Checked by: $*e=54.68 \left(\frac{b \times d}{a \times c}\right)$

or $e=15,833\left(\frac{d}{cxf}\right)$

DATA SH	EET 4	 OPERATING 	CONDITIONS	AND	CALCULATIONS
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					DATA	SHEE	T 4	- OPER	RATING	3 CO	NDITIONS	AND	CALCUL	ATIONS				
	FOIL NUMBERS	PRESSURE AT	GUN (KPa) ATOM, AIR		ATING RP		VOLTA	OPERAT IGE (RV)		. (MI?)	tenperati Ausient	PLUII		OOTH AIR TE (cm/s)	relative Humidity	GUN TO TARGET DISTANCE (cm)	CUITIME(a)	_
1644	176 187	1830	NA	NA	NI	4	N	A	N	A	20.5°C	247	BUC 1	0015	70%	ion	15m	(325)
0338	NZ 187	1810									20.52	26.	90 10	10+15	70%	10 m	15m	(223%
		1840									20.50	-25	62/1	offs	80%	10 m	15 n	375)
1865	194 199	1800			4		\perp		\dashv		21.0°C	25.	6% 10	soft Ls	74%	10 in	ISm	3150
01449	200 205	1830			11	_	1		\bot	_	91.00	266	, or K	xxHs	69%	10m	151	3250
1489	206 ZI	1840	1	V			1		1		21.0°(رعدر	P 10	OHB	62%	10in	Sm	<i>3759</i>
E-30				n	notin			£				<u> </u>	Ъ		c	đ	•	, •
Ü	POIL NUMBERS	VERTICAL COVERAGE (%)	PILM	DRY I	Redy Pl HIT. (9)	UID M ANIY	ASS F L (g)	LON RATE	DETERMENT	MINAT: ME(0)	ION RATE (q	3/e)	CONVEYO		EIGHT \	NET DRY SOLIDS (g)	Transf Efficien	
1644	to 176 181	15%	1.50 me	la) 3	SHO dr	M	<u>—</u> A_	128.9	, /	4,3	9.01g	39/1	40 CI i	n 5	7,40	21.47	46	, 1
838	to 182 197	18%	V.7n		rot/ ucndu			141.7	1 19	4,3	9.87	15	90 F/0	n. 5'	7,40	23.04	uS	1
	to 188 193	200/0	1.7.	rub 3	54/1/m			1292	3 1	7, 2	9.1 q. 596.		0 f/m	5	7.40	19.85	42	.7
			(.7mel	الم أ	-9/dh			142.	6 X	1.25	600		0f/n	5	7.40	23.09	44	1.7
	201)205	170/0	(Inc	0 5	545g/n			/30.0	0 14,	3	9.091	Sgrill	0 + lm		7.40	20.78	44	7
0	to	25%		< . h	557		,	137.0	14	4,2	1 4 2201	0	,		7.40	20.70	42	$\overline{\mathfrak{I}}$
1627	206 21)	7710	1, //-	<u></u>			<u></u>	12914		<u> </u>	124010	8 14	6f/n		7.40			

Data Collected by: 1918

Data Checked by: *e=54.68(bxd/axc

or $e=15,833\left(\frac{d}{cxf}\right)$

	FOIL NUMBERS	PRESSURE AT	GUN (KPa) ATOM,AIR		TING RPS D W/O FLUI	D VOLT	OPERA' AGE (RV)	ting Resi st. (M	TEMPERAT	URE (°C)				CURE TIME(a) TEMP (°C	
UILA9	8/2 2/7	1840	MA	NI	1/1) Λ	//A	NA	a/oc	25.	8 1001	14.62%	10in	15m 375	1
60865	408 223	1810							a joc	35.	8 1009	4 62%	10~	15m 375	
41649	to 444 429	1840							21.58	25.	8 100F	1/2 61%	10 in	15M 375	1
616 29	430 235	1840							21.5%	as .	8 100 p	1/4 6/%	10 m	15m 375	1
61649	to 236, 24/	1840							21.52	25.8	PDOG S	In 41%	10 in	1517 375	
61644	to HL H	1890	_\	V				1	91.50	25.8	32 100A	the 61%	10 m	15h 375	
E-31	r———			10	1691		f	·		<u> </u>	ь	С	đ	••	1
:	Poil Numbers	VERTICAL COVERAGE (*) PILM		PLUII MT. (g) P	HASS HAL (9	FLOW RAT	e deterhin) time(CONVEYOR PEED (cm/e)	Weight \ Solids	NET DRY SOLIDS (g)	Transfer Efficiency (4)	
41649	217217	20%	5 .7 m	ا دا	689h	v]a	135	8 14.3	9,449	15 79/2	40 f/m	57.4	ZI. 16	43.11	
60865	to 318 223	30°/	.6.	mila	00g/n		143.	8 14.3		Tal	70 F/m	57.4	22.77	44.0	
61649	229229	22º/6	1.7	mb	569g/m		135.	7 14.2		791	40 F/n	57.4	20,99	42.6	
l l		00%		5	5 84/m		133	3 14,3	9,30	30	tofun	57.4	19.31	40.1	For Chil
61649	to 24/	23%	.70	2 21.10	66g/m		135.	8 14.3	9.49	a/m 4	oun	574	2136	43.5	
61649		25%	7/	ib 5	44g/m	V	139	8 14.	9,07 594	1 11 4	of/m	57.4	zo.34	43.4	
1	Data Co	llected b	y: 000	-	7				() Da	ata Checke	d by:	*e=54.6	$B\left(\frac{b \times d}{a \times c}\right)$	
												0	r e=15,8	$33\left(\frac{d}{cxf}\right)$	

or $e=15,833\left(\frac{d}{c \times f}\right)$

DATA SHEET 4 - OPERATING CONDITIONS AND CALCULAT	TONG
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	Poil Numbers	Pressure at Fluid/ps;			PATING RPI		VOLTAG	OPERAT GE (RV)	'ing Resi st. (M Ω)	Temperat Ambient	ure (°C		AIR REL N/0) HUM	ATIVE	gun to tar Distance	RGET (cm)	CUITIME (D)	
4 16 99	248 255	1890	MA	AP!	M		MA	r	MA.	224	26	,5 1004	14 7-	2%	"10m	_	15n	375
61644	to 294 159	1890								22°C		SE 100 f		2%	100i		15m	375
61644	to 265	1440								2200	Zirle.	30,000	4/n 7	2%	10 m		15m	375
61619	to 246 27/	, ,								2200	36.	OC SOU PS	m 72	· %	10 in		15m	375
60865	272 27	1810								22°C	25.	8°C 1001.1	m 72	10	10 m		15m	375
UK32	213 283	6+1890		V	\		1		V	220	25.8	C 100f	11. 72	20/0	10 cm		15m	375
E-32	·		· · · · · · · · · · · · · · · · · · ·				,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	£				b	c		4		(• •
				1 4	LIA. EE'	_										•		
	Poil Numbers	VERTICAL COVERAGE (1)	WET C	DRY 1	N IT. (g)	HIT INIT	Mass Pi Al (g)	LOM RATE & (g)	DETERMINAT	rion Rate (g/a)	CONVETOR SPEED (CR/s)	WEIGHT SOLID	- '	NET DRY SOLIDS (TRANS EFFICIE	
51649			(,) rue	DRY	5659/n	S I H	AL 19)	A (g)	A TIME (S)	9.56	2/5		SOLID	08	•	g)		NCY (%)
	NUMBERS to	COVERAGE (%)	(WET)	US)		S I H	AL 19)	B (9)	14.3	9.56	9/5 694	SPEED (cm/s)	SOLID	l L	SOLIDS (2	efficie	8 8
61644	to 248 15.3	30%	(Jun	ds)	51.5g/n	S I H	AL 19)	134.7	7 14.3 14.3	9.56 (573; 9.11 q 544; 1.099 545	9/5 69/5 1/5 1/5 1/5	FOF/M	5 7.4)	21.1;	41 2 a)	47. 43	8 8
61614 61614	to 246 153 to 254 259 to	30% 30%	17m	ds)	545g/m	S I H	AL 19)	136.7	14.3 14.3 14.3	9.56 (573; 9.11 q. 5469; 5.45	9/5 (calc) 17/5/5 1/5/5	50 f/m 50 f/m	50L10 574 57.4	1 1 1	21.1; ZO.	11 11 2	47. 43.	8 .3
61649 61644	to 248 153 to 254 259 to 260 265	30% 30% 30%	17 mm	ds)	Str5glm 545glm 54loglm	S I H	AL 19)	130.7	14.3 14.3 14.3 14.3	9.56 (573; 9.11 q 5469; 5.099 5.45	9/5 1/5/5 1/5 1/5 1/5 1/5 1/5 1/5 1/5 1/5	40 f/m	57.4 57.4 57.4	4 4 4	ZO.1	5 41 11	42 43 47	8 3 2 8
61649 61644 60865	to 248 15.3 to 254 259 to 265 265 to 26,5 to 27,1 27,7 27,7	30% 30% 30% 18% 88%	17 mm 17 mm 17 mm 17 mm 17 mm 18 mm 17 mm 18 mm	ds)	Str5glm 545glm 546glm 546glm	S I H	AL 19)	130.1	14.3 14.3 14.3 14.3 14.3	9.56 (573; 9.11 q 5463; 1.099 545 7.099 5 45 10.0 9.06	9/5 15/5 15/5 15/5 15/5 15/5 15/5 15/5 1	90 f/m 90 f/m 90 f/m 40 f/m	5 7.4 5 7.4 5 7.4 5 7.4	+ + + + +	21.13 20.4 20.4	9) 5 41 11 12	42 43 47	8 3.9 4,3
61649 61649 60865 61632	to 248 153 to 254 259 to 265 265 to 271 277 to 278 283	30% 30% 30% 18% 24% 24%	17 mm. 17 mm. 17 mm. 17 mm. 19	ds)	Str5glm 545glm 546glm 546glm	S I H	AL 19)	130.1 130.1 130.0	14.3 14.3 14.3 14.3 14.3	9.56 (573; 9.11 q 5463; 1.099 545 7.099 5 45 10.0 9.06	9/5 15/5 15/5 15/5 15/5 15/5 15/5 15/5 1	90 f/m 90 f/m 90 f/m 40 f/m	57.4 57.4 57.4 57.6 57.6	+ + + + +	20.1 20.1 20.1 20.1	5 11 12 92 8	42 43 47 47 49	8 3 2 8 3.9 1,3

LABORATORY 2

Airless Gunlo37

i		O				D	ATA SHE	ET 4							
	Run Ho.	Gun Mo.	roll Mo.'s	Pressure Pluid	at Oun	Operati Voltage (kV)	=	Tempera	eture ^{C)} Pluid	Booth Air Rate (cm/s)	Pelative Mumidity	Contro Supply Alr	ol Panel Pr Atom. Air	essures Paint Pot	Air Flow (actm)
)	5	163		1805	NIA	NJA	NA	795	ッチ	80 - 100 41/5	59%	NA	NIA	NA	NA
40	1	163	3 7-6	1825				TAF	7195	80100	59%				F
00	a	163:	7-12	1825				76'A	<i>ኤ</i> ን	80 700	59%				
15	3	1632	13-18	1835				160	76.6	80-100	41%				
:30		1632	19-24	1825				1/2	16°F	80-100	£%				
:47	5	K32	25-30	1825	\bigvee			74°F	74°F	ЮJ00	58%	V	V	V	
!	Run No.	Vert. Thic		Fluid Total Hass (g)	CONCIL	A_Rate (gle	Con	Veyor Spee (cm/e)	d	w. o	Het Dry Solide (g		Transfer I		
	D	25% H	, ,	164.)	MARA		n A	0 Hs 995616	34, 5	58.09					-
1	1	350 N/	2 530g	WA. 1	WA	\$ 30g/		51010	4	75.05×		-			_
		30%	5289/	130.99	14.55		7/5 a.	975 Fel 52 (14)	_ ا	8.09	20.98	9 =		46.0	
	3/	49 .	530g/	NIM	NIN	53020	3.0	1824+	10 5	8.09	22.26		18-05	11	9 di

Data By

528dm 133/

Data Checked By:

31.689 45.73

Date: July 30 1985

Airless Gun 1632

DATA SHEET 4

	Run No.	Qun Ho.	Poil No.'s	Proceure Pluig	at Oun	Operati Voltáge (kV)	_	Temperat Booth (°C)	rluid	Booth Air Pate (cm/s)	Pelative Munidity	Control Bupply Air	Panel Pro Atom. Air	essures Peint Pot	Air Plow (acfs)
16:00	6	1632	31-36	1825	NIA	MA	MA	ZAOF.	7 1 %	1	61%	l t	NA	MA	NA
6:15	7	63 3	37-42	1825				71%	71°F		610%				
											·				
					V	1	\bigvee					V	1	\bigvee	

Vert.	Thick. Wet Pilm (mile)	Plow Rate	Fluid Has Total Mass (g)	rime (a)	Rate (gls)	Conveyor Speed (cm/s)	Wt. 4 Solids	Net Dry Bolidg (g)	Transfer Efficiency
48	8	U. C		15.155	0.983 = 530almi	298 4	58.09	a05d	44.76
10/40	.8	Salgn	34.4	15.40s	2527/10	2.995/24	58.09	20.63	45.097
			·				•		
						,			
	12/48 10/	(a(1e) (Z/45 /8	Plow Rate (mile) Plow Rate (pla) (R) 8 330g/m (O) 507644	Wort. Not Pila Plou Rate Potal Name (g) 12 8 530g/m 1308g 10 507644	12 (allo) Plow Rate Name (g) Time (n) 12 18 330g/m 1308g 15.155	Vert. let Film Plov Rate Total Doverage (mile) Plov Rate (g) Time (e) Rate (gle) [2] 530g/m 1308g 15.155 0.985	Vert. set Pila Plov Rate Total Plov Rate (g) Pine (e) Rate (gle) Conveyor speed (cate) (gla) 130/89 15.155 0.983 251 301.46 27	Vert. let Film Price Rate Total Doverage (a(1e) Fine Rate (g) Fine (e) Rate (gle) Conveyor Speed (ca/e) Solide [2] 8 530g/m 1308g 15.155 2.983 257 301.46 27 58.09	Vort. let Fila Plow Rate Rate (g) Fila (a) Rate (gla) Conveyor Speed Nr. 6 Rate (gla) (ca/a) Solida Solida Solida Solida Solida S

Data By:

Data Checked By:____

 $e=54.68\left(\frac{bxd}{axc}\right)$

or e=15,833 $\left(\frac{d}{cxf}\right)$

Date: July3/

DATA SHEET 4 Cues 2365

Run Mo.	Vert.	Thick. Het Film (mile)	Heter Flow Rate	Pluid Ma Total Mass (g)	ee Flow	Rate (gls)	Conveyor Speed (cm/s)	₩. 4 Solids	Het Dry Solide (g)	Transfer Efficiency
+	NR	M	2679/	1.36g	NIM	do Tylm	6.015/24	50%		>
2	34/ ₁₈₈	.7	3634m	191,29	31.55	1	5.975/24	50%	4.02	<i>45.87</i>
3	35/ ₄₈	.7	363/1/4	191,0	31.50	6.05g/5	5.49.V2F+	50%	14.38	26.45
4	37/18	;7	362g/	1892	NR	6.03-15	5.975/24	\$2%	13.70	a5.37
5	36/40	・フ	359g/m	186.6	NR	4.02315	6.02/25+	\$%	13.77	75.33
6	38/	507	369ly	184.5	30.73	6.00815	6.01/zft	D'/0	13.5/	24.98

 $e = 54.68 \left(\frac{b \times d}{2 \times c} \right)$

Data By: SPB

Data Checked By:

or $e=15,833 \left(\frac{d}{275} \right)$

Convertinal and DG5	-
DAMA CITYON A	

Pun No.	Gun Ho.	Poil No.'s	Procesure Pluig	at Oun	Volte	Operati ge (kV)	ing Cutr	ont (Temper Booth	ature ^{C)} Pluid	Booth Air Rate (cm/s)	Relative Humidity	Control Supply Air	Panel Pro Atom. Air	esures Paint Pot	Air flow (acfm)	1/ofull
7	1365	79 - 84	10ps 1	20 ps,	M	A	L	IA	791	797	85-100	50%	10	41.5	26/2	42.5%	% fuel 11.48+,
					1												
										· · · · · · · · · · · · · · · · · · ·							
				. 		/		,									<u> </u>
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Rain No.	Vert. Doyerage	Thick. Mot Pilm (mile)	Meter Flow Rate	Fluid Pa Total Mass (g)	oo Flow Time (a)	Rate (gle)	Conveyor Speed (cm/s)	Mt. 1 Solide	Not Dry Solids (g)	Transfer Efficiency
7	374	.7	360g/m	1829	NR	6.0	G025/244	50%		25.85
	,		J	0						

 $e=54.68\left(\frac{bxd}{axc}\right)$

or $e=15,833\left(\frac{d}{cv^{\epsilon}}\right)$

Data Checked By:

Date: 1/3//85

Clictrostatic Gun 1365
DATA SHEET 4

	Pun Ho.	Quin No.	Poil No.'s	Pressure	at Gun	Operati Voltage(kV)	•	Temper Booth	ature ^{C)} Pluid	Booth Air Rate (cm/s)	Polative Bunidity	Control Supply Alt	Panel Pre Atom. Air_	Point Point Pot	Air Flow (acfm)	% Full (1.4)
3:55	-8	1365	85-90		80 ps i	74 KU		74°F	749	100 100	91%	104	120	76.6	1240	
4:15	9	1365	91-96	NPS,	80,751	74	35	75°F	79F	80 1485/1	80%	102	A2	26.6	42%	
1:55	10	1365	97-102	10 psi	aopsi	74	35	759	-75°F	MACH	41%	104	4z	26.6	42)
5:05	//	1365	103 -	י בקט	20751	74	55	15.5	75.5	400 400	81%	104	42	24.6	4 2,	5
7:35	12	1365	109	ו זק 0ו	20751	74	35	74.5	74.0	80 H	81%	64	42	26.60	42	
5:55	13	1345	115	10.751	20,051	74	3 S	<i>7</i> 4.5	740	SOFT	81	100	42	26.6	42	

Run No.	Vert.	Thick. Wet Film (mile)	Meter Flow Rate	Pluid Ha Total Mass (g)	ss Flow Time (s)	Rate (gle)	Conveyor Speed (cm/s)	W. 4 Solide	Net Dry Solids (g)	Transfer Efficiency
8	42/48	9	360	1995	NR	36/ 6.0/g	6.055/2Ft	50%	47.77	87.62
9	43/X	4	361/40	199 D	NR	36/2-601	6.055/24	50%	48.05	88.1
10	44/45	16	341/40	199	RVR	361/601	6.015/25+	\$ %	45.01	8 2.6
1/	45/18	ں.	359/100	180	MR	359 5.18	6.015/aff	50 %	45.09	89.0
13	46/98	٧٠	359/	173.8	NR	359/60	6.02/2ft	56%	44.75	86.6
13	44 148	۵.	359	178	NR	359/60	6.03/24	50%	41.97	88.7

x = 86 3

5=2.91

 $e=54.68\left(\frac{bxd}{axc}\right)$ or $e=15.833\left(\frac{d}{cxe}\right)$

Data By: AFB

LABORATORY 3

Rush Ho.	Que No.	Poil No.ºs	Proseure Pluig	at Oun	Operati	-	Tempe Booth	ature ^{C)} Pluid	Booth Air Rate (cm/s)	Relative Bunidity	Control Supply Air	Panel Pre Atom. Air	eeuree Paint Pot	Air Flow (scfm)
/	61699	1-6	1825	NA.	קטק	NA	12,2	26,7	60.96		NA	NA	NA	
3		13-18	1825	NA	NA				60.96	j				
4		19-24	1825	NA	NA	NA	22,2	26:7	60.96		NA	NA	NA	
5.		<u> 25- 30</u>	1825	, •					60,96					
6		E1-26		·		•			,					
7		37-42	•	*					60.96					

Run No.	Vert. Doverage	Thick. Wet Film (mile)	Heter Flow Rate	Pluid Na Total Mass (g)	es Flow Time (e)) Rate ⁽⁾ (gla)	d Conveyor Speed (cm/e)	C Nt. 8 Solids	b int bry solids (a)	e Transfer Efficiency (1)
/	/ユ"	8	569	175.7	16.6	10.64	20.15	.52,96	18,04	35,27
3	/a"	d,	567	188,7	16,6	11.37	2015	52,96	18.79	34.38
1	12	8	567	200,6	16.6	12.08	20.15	52.96	19.13	32,95
5	12"	8	565	201.2	16.6	12.12	20,15	52.96	18,24	21,31
.,	12"	8	569	1929	16.29					
7	12	8	575	196.7	16.6	11.85	20,15	52,96	19.13	33.58

Date	:

Run No.	Que No.	Poll Wo.'s	Proceure Pluia		Operati Voltāge(kV)	ng Current (Tempes Booth	eture ^{C)} Pluíd	Booth Air Rate (cm/s)	Polative Munidity	Control Supply Air	Panel Pro Atom, Air	Paint Paint Pot	Air Plow (acfm)
8	61649	13-18	1825	NP	NA	קנו			60.96	 				
				•										
													,	
				•		•					•			
									•					

Run No.	Vert. Daverage	Thick. Mot Film (mile)	Heter Flow Rate	Fluid Na Total Mass (g)	es flow fine (s)) Mate (gle)	d Conveyor Speed (cm/s)	C Mr. 9 Bolide	b Not Dry Solids (g)	e Transfer Efficiency (1)	
8	/2"	7	570	194.9	15.95	12.22	21.02	55.21	18.09	20,81	men 1.73
											73
											mus= 1.
											•
											$^{+e=54.68}\left(\frac{bxd}{axc}\right)$

 $^{\bullet}e=54.68\left(\frac{bxd}{axc}\right)$

Data By:

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Run Ho.	Gun Mo.	Foll Wo. *s		Pressure at Oun Pluid Atom, Air 18		Current	Tempe	ature ^{C)} Pluíd	Booth Air Rate (cm/s)	Relative Munidity	Control Bupply Air	Panel Pre Atom. Air	Pot Paint Pot	Air Flow (acfa)
9	C-1355	49-54	9 DH	20	74	19	29.8 23.9	23.3	55.88	5170	93.5	40.5	240	39.0
10	C-1355	55-60	/1.75	20	74	29	23,8	29.3	55.88	51	87.0	410	240	39,a
//	C-1355	61-66	9.5	20	24	29	23.8	23.3	55.88	51	800	42.0	22.0	39.0
12	C-1355	67-72	9.5	20	74	29	23.8	23,3	55.88	51	80,0	42.0	220	39.0
13	C-1355	73-78	11.25	20	74.	29	Z\$.8	2 3 .3	55,88	51	820	42.5	22.0	39.0
14	C-1355	79-84	10.0	20	74	29	238	23.3	55.88	51	84.0	420	23.0	39.0

Ran No.	Vert. Poverage	Thick. Hot 7ilm (mile)	Heter Plow Rate	Pluid No Total Mass (g)	time_(e)	Pate a (gls)	d Conveyor Speed (cm/s)	C Mr. 6 Bolids	b .let Dry \$011de (a)	e Transfer Efficiency	
9	27	7	<i>‡8</i> 4	142.1	29.91	4.75	10.18	47.35	66.02	65.39 54.28	DN -
10	27	7	353	174.7	29.36	5,95	10.18	47.35	35.45	70.04	outher
11	27	b	300	148.4	29.70	5,00	10,20	47.35	27.95	65.84	16.95 20.95
12	27	6	301	150.6	29.63	5.08	10.20	47.35	28,10	65.16	mor =
13	27	7	354	177.2	30.81	5.74	10.20	97.35	33.02	67.76	
14	27	7	310	152.1	29.58	5.14	10.20	47.35	<i>19.08</i>	66.64	*e=54.68(bxd)

Data By: DSM

Data Checked Ru

DATA SHEET 4

Rus No.	Gun Ho.	Poll Wo.'s	Pressur Pluig	e at Oun	Operati Voltáge (kV)	ag Current (Temps Booth	ature C) _{Pluid}	Booth Air Rate (cm/s)	Relative Bunidity	Control Supply Air	Panel Pro Atom. Air	esures Paint Pot	Air Plow (actn)
15	C-1355	85-90	9.5	20	74	19	23.8	23.3	55.88	51	84	42	22.5	39
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	DINETAGO		Notes Flow Rate	Fluid Na Total Mass (g)	Time (e)) Rato ⁽⁾ (gle)	d Conveyor Speed (cm/s)	C Nt. 9 Solids	b Net Dry Solids (a)	E Transfer Efficiency (1)
15	27	6	285	141.5	29.62	4.78	10.16	47.35	26.97	66.20
						:		• .		
							,	•		

 $e=54.68 \left(\frac{b \times d}{a \times c}\right)$

Data By:____

		1
Com	entrona	C

Run No.	Cun Mo.	roil wo.'s	Pressure Pluid	at Oun			Temper Sooth	ature C) Pluid	Booth Air Rate (cm/e)	Poletive Bunidity	Control Supply Air	Panel Pro Atom. Air	paint Paint Pot	Air Flow (acfn)
16	C-1355	91-96	10.5	20.0	NA	NA	23.8	<i>23</i> ,3	55.88	51	82	42	22.0	39
17	C-1355	97-102	10.0	20.0	NA	NA	23,8	23,3	<i>55.</i> 88	51	82	42	23.0	39
18	C-1355	103-108	10.5	20.0	NA	NA	23.8	23.3	55.88	51	82	43	22.5	39
19	C-1355	109-114	10.5	20.0	NA	NA	23.8	233	<i>55.</i> 88	51	82	43	222	39
20	C-1355	115-120	10.5	20.0	NA	NA	z3.8	23.3	<i>55.88</i>	51	82	43	23.0	39
al	C-1355	121-126	10.5	20.0	NA	NA	Z\$.8	25.3	55.88	51	81	44	23.0	39

Run No.	Vert. Doverage	Thick. Mot Film (mile)	Motes Flow Rate	Fluid Ha Total Hass (g)	time (a)	hate ³ (ale)	d Conveyor Speed (cn/s)	C. W. b Solida	h Net bry Solide (e)	e Transfer Efficiency	
16	21	6	308	153.4	29.65	5.17	10.16	47.35	10.98	24.92	4
17	21	6	3/3	155.3	29.56	5.25	10.16	4-7.35	11.28	25.21	ween= 24.34 0.58
18	21	5	311	153.7	29.62	5.19	10.14	47.35	10.61	23.98	week 5.
19	21	5	309	151.1	29.01	5.21	10.16	47.35	10.64	23,96	
20	21	5	309	1523	39.22	5.21	10.18	4235	10.54	23.78	
21	21	6	310	154.0	30.29	5.08	10.16	47.35	10.48	24.20	$e=54.68\left(\frac{b\times d}{a\times c}\right)$

 $e=54.68\left(\frac{b\times d}{a\times c}\right)$

Data By:

Data Checked Rus

LABORATORY 4

anlice

Run No.	Que No.	roll No.'s	Procoure Pluid	at Cum	Voltage(kV) Current(Tempe g	ature ^{C)} Fluid	Booth Air Rate (cm/s)	70 Relative Munidity	Control Supply Air	Panel Pre Atom. Air	ssures Paint Pot	Air Flow (acful
/	1.829	1-6	1825	NA	NA.	NA	23.2 (73.7		50.8	56	NA	NA	NA	NA
2	12822	7-12	1850	NA	RU				50.8	45.5	NA	NA	AU	NA
,3	10859	13-18	1850	NA	NA	NA	22.7	21.6	50.8	46.0	NA	NA	NA	פמ
4	60879	19-24	1825	N A	NA	NA	22.7	21.6	50.8	460	NA	NA	NA	NA
.5	60827	25-30	1860	NA	NA.	·NA	22.7	21.6	50.8	46,0	NA	NA	NA	NA
6	fag34	31-36	1860	NA	NA	NA	27.7	21.6	50,8	46.0	NA	NA	NA	NA

RAIR No.	Wert, Doyerage	Thick. Wet Pilm (mile)	Motor Plow Rate	Fluid Na Total Mass (g)	oe Ylow Time (a)	Rate (gls)	d Conveyor Speed (cm/s)	C M. Solids	b Net Dry Solide (a)	e Transfer Efficiency
1	9,5	/4	490	115.0	14.41	7,98	22,21	58.76	19.07	49.39
7	80	90	580	144.8	14.45	10.02	22,15	58.76	23.08	47.48
	8.0	10	539	133.6	14.80	902	21.62	58.76	20.11	14.85
1 1	8.0	8	552	131.4	14.24	9.24	22,47	58.76	21.45	48.59
5	80	8	560	134,0	14,36	9,33	22,29	58,76	20.86	46,38
1	8.0	8	507	1175	14.23	-8,26	22.49	58.76	20.91	-5298

outlier
*e=54.68(bxd)

Data By:

Data Checked Rus

i Shun Ho.	Que No.	Poil No.'s	Processo Pluid	at Oun	Operati Voltáge(kV)	•	Temps (eture ^{C)} Pluid	Booth Air Rate (cm/s)	Relative Humidity	Control Supply Air	Panel Pro Atom. Air	esuree Paint Pot	Air Flow (scfn)
2	60829	37-42	1825	NA	NA	NA	<u>23.3</u>	21.6	50.8	45,0	NA	NA	NA	NA
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Russ Ito.	Vert. Dyrerage	thick. Wet Film (mile)	Meter Plow Rate	Finid He Total Hess (g)	on Flow Fine (a)) Rata ⁽⁾ (gle)	d Conveyor Speed (cm/s)	C W. 0 Solids	b Net Dry Solide (a)	e Transfer Efficiency
2	80	8	482,0	116.7	14.43	8.09	22.18	58.76	19.76	50,53
	1							• .		
										-

Data By:

Data Checked Rus

Conventional

Rus No.	Que No.	roil We.'s	Pressure at Oun Pluig Atom, Air V		Operati Voltāga(hV)	-	Temper Sooth	eture C) Fluid	Booth Air Rate (cm/s)	Polative Munidity	Control Supply Air	Panel Pre Atom. Air	asures Paint Pot	Air Flow (acfm)
14	(-1336	77-27	9.75	20	NA	NA	227	22.S	55.7	11	90	19	.ZR.5	72
	•	85-90		20	R'A	NA	27,7	22.S	55.9	11	87	13	27.8	72
		91-96		70	N' /7	N'A	22.7	22.5	55.9	11	88	43	21.8	13
		17-162		iii	L'A	NA	22,7	72.8	55.9	14	90	44	27.8	73
		163.168		•	N'17.					41	90	45,5	280	73
19	C-1336	107-119	9.75	20	NA	NA	22.7	22,S	55.9	44	87	45.5	28.0	73

RMA No.	Vert. Doverage	Thick. Hot film (mile)	Heter Flow Rate	Tiuid Ha Total Hass (g)	oo 71aw Timo (a)	} Rato (gls)	d Conveyor Speed (cm/s)	C W. & Solide	b Net Day Solids (a)	e Transfer Efficiency (1)	
14-	21"	8	340	1846	28,21	6.54	10,26	18,77	21.53	39.63	DB -
15	al"	8	391	184.9	28.28	654	10.23	48.77	22,47	39,44	
16	31	g	393	185.5	.28.24	651	10,25			3902	
11	21	8	393				10.19	,		39,17	
18	<i>\$1</i>	8	573		28.44		10.18	1			(1%)
19	21	8	388	185.0	23,56	6.48	10.14	48.71	21.98	38.56	*e=54,

Data By:

Data Checked Ru:

 $e=54.68\left(\frac{bxd}{axc}\right)$

Run Ho.	Que No.	Poil No.'s	Procesure Pluia	at Oun	Operati Voltāga(kV)		Temper Booth	ature ^{C)} Pluid	Booth Air Rate (cm/s)	Relative Bunidity	Control Supply Air	Panel Pro Atom. Air	Paint Pot	Air (
8	C-1330	43-45	10	20	74	10	233	22,8	85.9	44	joc	45	30	72
9	2-1996	19-54	10	20	74	10	233	22.8	55.9	44	89	72	24	71
16	C-1336	55.60	9.75	20	71	2.5	233	223	559	44	85	44	ત્રેશ	7.2.
<i>i1</i>	(-1236	61-66	10.0	20	71	25	:7.1	<i>4</i> 3.8	55.9	44	90	45	30	71
		(7-12	:	20	74.	. 24	22.7	22.8	55.9	44	87	14	29	71
19	C-1536	73-78	10.0	20	74	24.4	22.7	22.5	559	44	59	45	27.8	71

Rasi No.	Vert. Doverage	Thick. Wet Film (mile)	Notes Flow Rate	Fluid Ha Total Hass (g)	PE Flow Time (s)) Pata (gla)	d Conveyor Speed (cm/s)	C Mt. 6 Solide	b Net Dry Solids (a)	e Transfer Efficiency	
8	Z4"	8	423	204.6	28.88	708	10.02	48.77	43.37	68.11	10.85
9	24	8	400	197.2	29.48	6,52	9.83	48.27	12,14	71.17	
10	21	8	380	187.8	27.02	6,97	9.98	18.27	40.62	70.23	Mesan 1.30
11	2.4	3	339	187.0	28.71	651	10,03	48.77	10:18	70.79	
18	30	ς	341	186.6	2866	6.51	10.10	48.77	1.11	12.55	
13	21	<i>?</i>	391	1860	28.44	6.54	10.18	18.77	41.03	71.60	$e=54.68\left(\frac{b\times d}{a\times c}\right)$

Data By:

Data Checked Ru:

LABORATORY 5

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Rea No.	Can to.	Pell Wo.'s	Proseure Pluid	at Con Atom, Alf	Operation (NY)	_	Tempeg Booth	iture ⁽¹⁾ Pluid	Booth Air Ante (cm/s)	Relative Healdity	Control Supply Air	Panel Pr Atom. Air	Pot	Air Flow (sets)
1	60865	1-6	1825	NA			250							
2		7-12					25.0							·
3		13-18			·		250							
4		19-24		NA			250							
5	11	25-30		NA	<u> </u>		25.0							
6	"	36-36					25.1					 -		

l i	Wet.	Thick. Not Film (mllo)	Notor (Piuld Na Potal Nace (g) f	time (e)	a mate (ab)	b . Conveyor Speed (cm/o)	C W. 1 Solide	Mex Dry Solide (a)	C Transfer Efficiency (9)
1	8"	6	590 33	139.5	/4.18	9.84	20:42	58.94	20,70	39.86
2	8"	8		139,3	14.08	9.89	20,54	58.94	21.82	42.08
3	8"	11		/43,7	14.81	9.10	19.55	58.94	20.60	38.51
4	4	€		131.6	13.24	9.44	21.87	58.94	17.13	36.492
5	£"	8		139,1	13.62	10.21	21.26	58.44	18.40	35.58
10	E	8		136.2	12.87	10.78	22.50	58.94	18.49	36.X1 5

X= 38.107 S= 2.534

e=54.68(bxd)

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Data Checked By: 78 8 Tright

r _=15,833 (d)

(muentienal (Electrosfatic nate up) Date: 124 DATA SHEET 4

Data By: NGS

Data Checked By: NGS

	Run Ho,	Que No.	Poll No.'s	Pressure Pluid	at Gum	Operati Voltāge(kV)	ng Current (,)	Temper Booth	ature C) _{Fluid}	Booth Air Rate (cm/s)	Relative Humidity	Control Supply Air	Panel Pro Atom. Alr	Paint Pot	Air Flow (scfm)
	13	C1320	73-76			NA				(70		150	SY	28.5	39
Electo State_>	14	4320	18-84			NA				lzo		132	42	38.6	39
	เร	C1320	85-90			NA				121		123	42	38.8	39
	16	81320	91-96			MA		/		1/21	\	150	MZ	38.8	39
JOND	17	C1520	17-162			MA				120		No	SY	28.8	39
E-52	18	c(370	103-108			NA	0.0			121		-		३५११ ०	

Mu182722

					_		1-3					
	Reals No.	West.	Thick. Wet Pile (mile)	Mater Plow Rate	Fluid Ha Total Hass (g)	es flow	((6) Rate (910) A	Conveyor Speed	et. 9 Solids	D Met Dry Solide (a)	Transfer Efficiency (1)	
	13	17	6	396	188.0	28.45	29.32	10.18	51.46	21.55 000.000 21.55	34.98	
Electrostic >	14	16.5	10	392.6	183.4	28. 11	6,52	10.30	51.96	41,78	69.42	< Electron Studio
	15	17	4	3926	183.9	28,10	6.54	10.30	51.96	21.53	2 - 73 7	
*	48	17	٩.	(189-2	28.90	6.55	10.02/	91.96	2	1	
X	17	17	9		182.7	27.84	6.56	10.40	51 96 /			1012
1 30 x	16	· · ·	",		783.2	2750	6.61	10.48	51.96	21.38	35.56	
	16	1	11		10 1.2	1	6,01	, , , ,		/ ////)	35,36	

	Rus No.	Que No.	Poll Po.'s	Presente Pluis	Operatio Voltace (LV)	_	Tempor	iture ^{C)} Fluid	Booth Air Anto (cm/s)	Relative Buildity	Control Supply Air	Panel Pro Atom. Air	Boures Point Pot	Air Flow (acts)
	19	C1320	107-114						120		122	42	·38.8	39
*	lb	(1520	91-96						121		150	42	38.8	39
*	17	432	97-102					٠	1 70		140	77	38.8	39
*	18	c1320	103-16					·	121		117	42	8.8	39
										•			****	
													transpositi	

,	1 i	Vert.	Thick. Mot Film (mile)	Notes Flow Nate a	Pluid Mar Total Mass (g) f	Time (a)	A Rate (ale)	D . Conveyor Speed . (cm/s)	C W. 6 Solide	d Not Dry Solida (a)	E Transfer Efficiency
	19		10		189.2	28.91	6.54	10.02	51.96	21.91	35.293
×	16		11	346.8	63. 2	27.70	6.61	16.45	51.96	21.38	35.86
×	180		10	392.8	189.7	28.98	6.55	10.02	51.96	21.21	34.162
*	R		9	393.757	1827	27.84	6,56	10,40	57.96	21.74	36.263
								-			
į	_ '					1				لــــــا	J

mac,-35.3 SD 0.72

 $e=54.68\left(\frac{bxd}{axc}\right)$

r 15,833 (d

a By: Data Checked By:

	Au No		. Po.	Poll Bo.'s	Presente Pluid	at Oun	Operati Voltāca(ty)	, -	Peoper S	ture	Booth Air Pate (cm/s)	Sulative Bunifity	Control Supply Air	Panel Pro Atom. Air	Pot_	Air Flow (actual	
		7	320	37-42	10	20	74	25			120 fpm		145	42	28,5	39	
	8		52G	43-48	10	20.	24	25			120		145	42	28.5	39	
	9	CI:	320	49-54	10	20	74	25			120		130	42	28.8	39	
	10) (1	326	75- 5 0	10	20	74	25			170		130	2 Y	28.6	39	
	1		326	61-66	10	20	74				0.00	•	117	42	58.6	39	
	16	Z CI	320	67-72	10	20	74	25			120		123	42	25.00	39	
	2 · ·	Vert.	Thick, not pil	Meter Flow Sate	Pluid H fotal H heas (g) f	Time (a)	A Pata (gla)		b reyer spec	•	C M. 1	d Het Dry Polide in		e Preseter t	fficiency		
	7	21	9	180.9	BIDH Ro.9	26,79	6.70	0 1	0.82	1	51.96	41.89	, -	10.50	56		
	B	2.1	8	400.77	185.9	27.83	6.68	s /	0.40		51.96	40.9	6	67. y	1		-
	1	21	8	385. 75	/83.3	28.51	6.4	3 10	5.16	4	51.96	41.4	4	8.8 3	19	5 =	1.1
	10	2,1	10	387.6	183.8	28.45	6.41	6 1	0.18		51.96	41.4	2	68.6	7		
0-	11/	X	9/	Nop	15.5.7	28.04	وكروا	5	10.33	, .	5496	46.5	3)]_f	6.2	YOID	5/6
	12	21	11	39718	185.0	27.90	6,6	3 1	0,38		51.96	42.3	0	69	67	*e=5	

Data By: DER/1954

Data Checked By SHIDB

LABORATORY 6

Rea No.	Can No.	rell to.*s	Prosoure Pluis	at Oun	Operati Voltace(hV)	•	Tempog Booth	eture ^{C)} pluid	Booth Air Bate (cm/s)	Polative Busidity	Control Supply Air	Panel Pro Atom, Air	eoures Paint Pot	Ale Flow (actual
	C0838	1-6	1850	N.A.	NA	NA	2 5 .8	78.8	55.88	10%	NA	NA	NA	NA
2	60038	7-12	1850	N A) .	NA	NA	28.8	28,8	55.88	7070	NA	NA	NA	NA
3	60838	13-18	1850	NA	NA	NA	28.8	28,8	55.88	70%	NA	NA	NA	NA
4	60838	19-24	1850	NA	NA	NA	288	28.8	55.88	70%	NA	ממ	NA	NA
5	60838	25-30	1860	NA	NA	NA	28.8	28,8	55.88	70%	NA	NA	NA	NA
6	60838	31-36	1850	NA	NA	NA	78.8	288	55.88	7076	NA	NA	NA	NA

**	Vert.	Thick. Mot Film (mile)	Motor Plan, Sato d	Field He Total Heas (g) #	Time (a)	a, note (sta)	b . Commyet Speed (co/s)	C W. 6 Polite	d Nev Dry Selida (a)	e Transfer Efficiency	
/	8"	7,0	509	120.3	/4.29	8.42 505.11	20,26	55,38	18.15 55.38	43.12	(12/2)
ವ	8	9,0	515	120.1	14.19	8.46	20,40	55,38	18.22 55.38	43.38	Y= 43.18
3	8	9.0	510	121.6	14.29	8.51	20,26	55,38	17.93 55.38	42.14	0.76
4	8"	9.0	509	126,5	14.91	8.48	18.42	55.38	19575 55,387	12,764	pr. 312 · ·
3	8	90	508	121.9	14.40	8.46	20.11	55.38	13.1.2 55.38	72.5X	X = A2.4 S=0.59
6	8"	8	510	122,6	19.47	. 8,51	20.01	55,38	18.81 55.38	43.6%	*a=54.68(bxd)
	a By:	Silve	$I_{}$	Data	Checked	By: OLA	4			0.1	$= 15,833 \left(\frac{d}{c \times f}\right)$

Electrostatic

Buildity	Dupply Ale	l Panel Pre Atom. Air	Pot Perus Pot	fice (pc(n)
45%	95	47	27	68
				68
ľ				
				68
·				68
			27	68
	457 457 457 957	457, 99 457, 105 457, 95 957, 89	457, 99 41 457, 105 44 457, 95 49	95% 105 44 27 95% 95 49 27 95% 89 44 27

20	Vort.	Thick. Mat Film (mile)	Noter Pley Note a	Fluid Hase Fl Total Hase (g) f Yim		(a)	b . Conveyor speed (co/e)	C UR. 5 Solido	d Not bey Solida (a)	Transfer Efficiency
7	26	7	380	184.7 2	9,15	6.34	9,93	53.0	43,55	70.37
8	26	7	375	181.3 2	9.06	6,23	9,96	53.0	43.21	71.27
9	26	7	373	179.8 2	8.89	6,22	10.02	53.0	43.19	71.78
10	26	2	369	178.4 28	8.97	6,16	10.00	53.0	42.57	71.30
"	3la	7	367	175.8 2	8,73	6,12	10.08	53,0	43.93	74.65
12	26	7	376	181,5 Z	8.94	. 6.27	10.00	53,0	42.08	69.24

X=71.445 S=1.44

 $e=54.68\left(\frac{b\times d}{a\times c}\right)$

1_a By: 152/

Data Checked By: Deli

or 15,833 (d ext)

Conventional

M te	Oun Ro.	roll Po.ºs	Process Fluid	et Own	Operation (NY)	•	Tempog Sooth		Booth Als Pate (cm/s)	helative Healdity	Control Supply Air	Penel Pro Atom, Air	epuree Point Pot	Air Flow (acfu)
13	C-1356	73-78	10	20	NA	NA	28,8	28,8	55.88	45	97	44	26,5	68
14	•	79-84	10	20	NA				55.88			44	26,5	68
15	,,	85-90	10	20	NA	NA	28.8	28.8	<i>55.</i> 88	45	100	44	26.5	68
16	"	91-96	10	20	NA				55.88	45	25	44	26.5	
17	<i>"</i> .	97-102	10	20	WA				<i>55.</i> 88	•	95	44	26,5	
18	11	103-118	10	20	NA	NA	28.8	28.8	55.88	45	101	44	26.5	68

2.	Wort.	Thick. Not Pila (mile)	Notes Flow Nate a	Fluid Me Total Mass (g) f		A mea (gla)	b Conveyed Speed (cs/s)	C W. 6 Solide	d not hay solide (a)	e Transfer Efficiency
13	25	5	371	176.8	28.58	6119	10.13	52,63	18.28	31.08
14	25	6	367	175.1	2864	6.11	10,11	<i>5</i> ⋥,43	18.13	31.19
	35		371	176.7	28.56	6.19	10.14	<i>ડ</i> ર.૬રૂ	18.70	31.83
14	25	7	366	174.6	28.66	6,09	10.10	52.63	17.91	30.86
17	25	7	254	168.9	28.59	5.91	10.13	52.63	17.22	30.26
18	25	7	362	174,3	28,86	.604	10.03	52.63	17.67	30.548

e=54.68(bxd)

Data By: ESH

Data Checked By:

or e=15,833 (d)

LABORATORY 7

DATA SHEET 4

Rus No.	Om No. Poll No.'s Prosours at Om Pluis Atom. Air			Operati Voltage (kV)	•	Tespe [ature ^{Ci} pluid	DA Scoth Air Pate (cm/s)	Polative Memidity	Control Supply Air	Panel Pro Atom. Air	seures Paint Pot	Air Flor (acts)	
/	61449	1-6	1825	NA	NA	NA	22.7	Z3 .9	55.88 4.66	65.5	ALR	NA	NA	NA
2		7-12	1825	1.	NA		22.7	23.9	55.88	8				
W		13-18	1825		תע		<i>2.7</i>	23.9	55.88	655				
4		19-24	1825		NA		:22:7	23.7	55.88 4.64	45,5				
5	DH	3 /-36 75 30	1825		NA		22,7	23,9	55.88 4.64	65.5				
6	6149	37-42 31-36	1825	$\sqrt{}$	NA	\downarrow	22,7	23.9	55.88	65,5	V		1	1

10	Wort.	Thick. Mot Film (mile)	Notes Plow, Nate a	Tivid Page Flow Total I Mass (g) f Fine (e)		Pate (gle)	D Conveyor Speed (cm/s)	C W. 6 Solide	d Not Dry Bolida (a)	E Transfer Efficiency
1	7	7	489	127.4	13.98	9.11	20.73	56.27	13.62	30.08
2	2	7	535	124.7	13,97	8.93	20.73	56.27	13.27	29.94
3	7	7	539		13.92		20.80		13.13	29,53
4	7	7	539	125.4	13.96	8.98	20.74	56,27	13.61	30.54
5	7	8	531	123.5	13.94	8.86			13.23	30.13
6	7	7	535	123,5	13.85	. 8.92	20,91	56,27	13.46	

 $\bar{X} = 30.15$ $\bar{5} = .9/13$

DATA SHEET 4

Refi No.	Cun No.	Poll Mo.'s	Presoure Pluid	•	Operati: Voltice (LV)	. , , ,		eture ^{Cl} pluid	Booth Air Bate (cm/s)	Polative Humidity	Control Supply Als	Panel Pro Atom. Air	peint Pot	Air Flow (actu)
2	2-1382	43-48	10	20	74	20	24,4	23.7	55.88 14.	71	105	48	38,5	14
8	1	49-54		20	74				55.88	7/	110	49	38,5	44
9		55-le	10	20	24				55.88		ilo	49	38,5	
10		61-66	/ ^	20	.74				55.88				38,5	
11		67-72		20	74				55.88	71	108		38,5	
12	V	73-78	10	20	74				55.88	71	108		38,5	

25.	Wort, Paretage	Thick. Mot Film (mile)	Noter Flow Nate a	Field Na Total Nass (g) f	oo 71au Timo (o)	Pate (gle)	b . Conveyor Speed (ca/s)	C W. 1 Solide	d Not bey Solida (a)	Premofor Efficiency	527
7	20	6	386			6.43	7#9.00 6.43	51.36	33.50	50.36	52,20
8	30	6		l		6.35	9.03	51.36	34.45	52.14	31.78
9	20.	6				6,38		51.36	33.18	51,22	ا لي <u>ج</u> ير ارتبار
10	20	6	383	204.1	32.06	6.38	9.03	· . 51.36	33,43	50.34	2-35 1.59 1 .87 3
1/	20	6	381	203,0	31.97	6.35	9.06	51.36	35.87	54.47° PB	
VZ	20	6	383	2043	37,64	. 6.38	9.04	51.36	36.22	54.65	*a=54.0
L	a By				Checked						. 15,0

or $15,833 \left(\frac{\text{d}}{\text{cxf}}\right)$

no.	Cun Ro.	Poll Bo.'s	Prosour		Operati Voltace(LV)	•	Tompog (ituro ⁽⁾ Pluid	Sooth Air Rate (cm/s)	Relative Residity	Control Supply Alr	Panal Pro Atom, Als	pauree Paint Pot	ALF Flow (acfn)
13	C-1382	79.84		20	NA	NA	23.3		55.88		108	49	28,2	44
14		85-90	10	20			23,3			77	108			
15		91-96	10	20			23,3			77	108	19	28,2	44
16		97-102	10	20	•		233			77	108	49	28.2	94
17		103-108	10	20			<i>233</i>			77	108	49	28.2	44
18	Y	109-124	10	20		4	23,3		4	77	108	49	28,2	94

=	Vort. Paracage	Thick. mt film (mile)	Hotor Plow, Rate & Laval Victor	Field to Total Mass (g) f		Pato (gle)	D Conveyor Speed (cm/s)	C R. 1 salide	d Not bey Solida (a)	<u>e</u> Transfer Efficiency
13	21,5	6	389	213.4	32.84	6.50	8.87	50.55	18-82	27.62
14	22,5		:			6,60	8.87	50,55	19.08	27.76
						6.63	8.86	50.55	20.06	20. 98
1 1		ı			32A0		8.94	50.55	19.85	28.543
1 1		i		ı	32.71		8.85	50.55	19.06	27.15
18	22,5	6	405	219,4	32,52	.6.75	8,90	50.55	19.54	27.90

 $e=54.68\left(\frac{b\times d}{a\times c}\right)$

Data By:

Data Checked Rvs

or e=15,833/d

LABORATORY 8

[T] 64

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DATA SHEET 4

Buth No.	Case No.	rell te. *s	Process Pluis		Operati Voltass(LV)	0	Teaper Booth (St.,,,,	Booth Air Date (cm/s)	Polative Menidity	Ale	Panel Pre Atom, Air	gauses Paint Pot	Air Flow (actu)	o and so
١	61644	1-6	1825	NA	NA	NA	2 3.8 75°	75°	190-120 Fem	21%	NA	NA	NA	NA.	-zone pones sol
7	61644	7-12	1825				,1	*1	4	42%					- gun solt
3	4644	13-18	1825				0 1	1)	8 9	(34%)					
4	61644	19-24	1825		•		75	75'	/1	25%					
5	61644	25-36	1875	·			"	")	11	-					
6	61644	31- 36	1825	1	1		75	B	18	25%	1	V	V	V	

7.	Vert. Dyerage	Thick. Mot Film (mile)	Hotor Flow Rate a	Field He Total Heas (g) f		Pate (gle)	b Conveyor speed (cm/s)	C R. 1 folide	d Not Dry Solida (a)	e Transfer Efficiency
1	7	9	500	125.3	15.12	8.28	20.32 Cmg	56.82	21.94	49.9
ι	7"	9	502	127.4	,		7	56.82	21.27	46.5
3	1	9	502	124,7	15.02	8.30	ti	56.82	21.80	48.7
4	7.	9	502	/24.9	1.(,	8:46	1)	56.82	21.37	47.7
5	7	9	512	126.6	_		11	56.82	21.89	48.2
6	7	9	529	133,3	15.37	867	h	56.82	21.15	44.2

Data Checked Bu-

or __=15,833/d

٠				• 1	_	-	Peopeg Booth	eture ^{Cl} pluid	Booth Air Rate (cm/s)	Polative Healdity	Control Supply Air	Panel Pro Atom. Air	Paint Pot	Alf Flow (sector)	
C-17			10	20	74 V	30	671	65		60%	84	43	12	68	
C-17			10	20	74	30				60	84	43	12		
C-1			10	•	74	30				60	84		12	69	
) C-1	790	55-60)							
	290	CA-66	18	20	74	<i>A</i>				60			12	70	
3 C-1	290	67-72	10	20	74	30		65		46	82	42	12		1
Vert.	Thick. Not Fil (mile)	Motor Plow Rate a	→	_	Pate (gle)	Com	reyor Spe	-4		d Not bry Selida (e)		e ranefer to	liciancy	5 wys	colus added
17	10	206	110,9					,	47.00	216	82		3 4	LL. 28	_
17	9	199	100.0	,						21-8-2 21-8-5	75	66.8	13.51	69.90	, ~ ^
17	9	205	107.2						47.00			مبرتها	51	68.00	5= h71
17	9	202	103.7				-		47.00°	22-11	o Mr	سطط	7131	71.99	Dm= 3
17	9	200	1119				, 1		47.00	27.8	2	68	or	(Averag	18.99)
17	9	200	107,1	/					47.00	21.90	0	69.	.07	*e=54	68(<u>p×q</u>)
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Development of Proposed Standard Test Method for Spray Painting Transfer Efficiency; Volume II. Verification Program	5. REPORT DATE April 1988 6. PERFORMING ORGANIZATION CODE						
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15. SUPPLEMENTARY NOTES AFFRI project officer is Charles	H Danvin Mail Drop 62h						

919/541-7633. Volume I describes laboratory development of the method.

The two-volume report gives results of a program to develop and verify a standardized spray-painting transfer-efficiency test method. Both review of the literature and laboratory research were conducted. Transfer efficiency measurement methods presently used by industry were evaluated and compared. The best characteristics of these methods were incorporated into the final proposed standard method. The resulting method was determined to be viable for laboratory evaluations. It still awaits adaptation and verification for production line applications.

17. KEY WORDS AND DOCUMENT ANALYSIS								
a. DESCRIPTORS	b. IDENTIFIERS/OPEN ENDED TERMS	c. COSATI Field/Group						
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Spray Painting	Stationary Sources	13H						
Tests	Transfer Efficiency	14B						
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