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Coal Conversion Control Technology Volume III. Economic Analysis; Appendix

Interagency Energy/Environment R&D Program Report

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Coal Conversion Control Technology Volume III. Economic Analysis; Appendix

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ABSTRACT

Information has been gathered on coal conversion process streams. Available and developing control technology has been evaluated in view of the requirements of present and proposed federal, state, regional and international environmental standards. The study indicates that it appears possible to evolve technology to reduce each of the components of each process stream to an environmentally acceptable level. The conclusion has also been reached that such an approach would be costly and difficult of execution.

Because all coal conversion processes are net users of water, liquid effluents need be treated only for recycling within the process, thus achieving essentially "zero discharge." Further, with available technology gaseous emissions can be controlled to meet present environmental standards, particulates can be controlled or eliminated and disposal of solid wastes can be managed to avoid deleterious environmental effects.

Volume I focuses on environmental regulations for gaseous, liquid, and solid wastes, and the control technology for liquid effluents. Volume II deals with the control technology of gaseous emissions and solid wastes.

Volume III includes a program for economic analysis of control technology and includes the appendix.

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SECTION 11

PROGRAM FOR ECONOMIC ANALYSIS OF CONTROL TECHNOLOGY

The overall program for economic analysis of control technology has as its objectives:

- Determination of capital and operating costs for individual control processes

- Assembly of cost models that consider control efficiency and the effects of conversion process plant size and location

- Development of the cost models as modules which can be added in various combinations to yield the total cost of environmental control for each of the selected coal conversion processes

It is the intent of this section of the project report to prioritize the work that is recommended for the economic analysis of available and developing control technology to include the following:

- Preparation of a list of existing and developing control technologies that can be considered as being usable for each specific known pollution problem in coal conversion plants

(*) Pages 523-888 are in Volume II; pages 1-522, in Volume I.

- In selecting control technology for economic evaluation, assignment of priorities to consider such factors as the importance of the pollutant, the probability that a specific control will be utilized, the availability of adequate information to permit economic evaluation, the adequacy of present economic data, and the availability of alternate controls

- Preparation of a list of control technologies recommended for economic evaluation

- Rationale for developing control technology that could replace the recommended control technologies

- Recommendations concerning which control processes should be considered for economic evaluation for environmental control for selected coal conversion processes

- An explanation of the cost estimating procedures to be used, the level of detail and the estimated accuracy

- Method for comparison of the cost for control with the total project cost

TREATMENT OF LIQUID EFFLUENTS FROM COAL CONVERSION

Streams to be Treated

Non-Oily Water Runoff--
Source is the storm water and washdown water from areas of the conversion plant that are not subject to oily spills and leaks. These areas are segregated by a separate ditch and collection system from the oily plant areas. The water is collected and,

without interim treatment, becomes part of the raw water feed to the conversion plant.

Oily Water Runoff--
Source is the storm water and washdown water from areas of the conversion plant subject to oily spills and leaks. These areas are segregated from the non-oily areas by a separate ditch and collection system. The collected water passes through an oil-water separator. The separated oil is collected and sent to the incinerator/boiler. The cleaned water joins the process quench condensate stream after the condensate stripper.

Coal Pile Runoff--
Storm water runoff is collected by a ditch and sump system and becomes part of the water stream to ash/slag quenching.

Solid Waste Disposal Runoff--
Source is the leachate from the solid waste disposal area which may be partly storm water runoff and partly drainage from the solid wastes. Collected at the disposal area into a sump, it is returned to the conversion plant to be used as ash/slag quench water.

Coal Pretreatment Scrubber Water--
Source is the scrubber for the coal dryer offgases in the coal preparation plant. The scrubber is usually a recirculating type and the small bleed or overflow stream, bearing some oil, is combined with the oily water runoff.

Boiler Ash, Superheater Ash--
Source is the utility boiler/incinerator. The ash is dry, or quenched with minimum water to cool it.

Gasifier Ash Slurry--
Quenched ash/slag from the gasifier is dewatered, combined with the boiler ash, and transported to disposal as a damp mass. The separated water is returned to the ash quenching pit for reuse.

Process Gas Quench Condensate--
Source is the gasification reactor offgas cooler. In Lurgi gasification the quench water contains large quantities of phenols, oils, and tars. In Bi-Gas gasification the content of phenols, oils, and tars in the quench water is so low that separate treatment is not required. In SRC liquefaction phenols, oils, and tars are present in sufficient quantity to require separate treatment.

For Lurgi and SRC quench condensates the waters pass through an oil-water separator. The tars and oils are collected and usually sent to the incinerator. The cleaned water passes to phenol extraction and then to sour water stripping.

Sour Waters--
Source is the condensates from cooling the gasification offgas after the gas has passed through the quenching step. These waters are combined and steam stripped to remove ammonia, carbon dioxide, and hydrogen sulfide. The stripped water in the Lurgi process is sent through air flotation to remove any remaining oil, the oil is sent to the incinerator and the clarified water is sent to biological oxidation. The stripped water from the liquefaction part of the SRC process requires a flocculation step before air flotation and biological oxidation, with the flocculator underflow being sent to the incinerator. In the Bi-Gas process and in the gasification part of the SRC process the process quench condensate is sour water and this passes directly to steam stripping. The stripped water may be returned to the cooling tower makeup water system or to the raw water treatment system.

Biological Oxidation Sludge--
Feed source is the stripped sour water in the Lurgi and SRC processes. Organic content of the water is reduced by biological action to such a level that when clarified and filtered it may be used as cooling tower makeup. Organic sludges are dewatered by filtration and sent to the incinerator or, possibly, to the gasifiers.

Utility Boiler Blowdown--
This water stream contains no organic or volatile materials and is therefore routinely sent to the cooling tower basin.

Cooling Tower Blowdown--
This stream contains suspended and dissolved inorganic salts. Treatment may be directed toward concentrating the stream by evaporation. Alternately, the blowdown may be treated in a sidestream treatment step, with clear water returning to the cooling tower and the more concentrated blowdown stream being sent to evaporation or other disposal.

Sludges and Brines from Makeup Water Treatment--
Source of the sludges is the chemical precipitation steps of the raw and recycled water treatment sequence. Source of the brines is the demineralizing step that follows chemical precipitation and, if used, the reverse osmosis treatment step. Dissolved and suspended inorganic salts may be concentrated by evaporation or be combined with ash to be sent to disposal.

Methods of Treatment

It is seen from the foregoing that each stream is treated to the extent necessary to prepare it for reuse in the conversion process. The contaminants that are removed from the wastewaters appear as saleable products (ammonia, phenol), as gases (carbon

dioxide, hydrogen sulfide), or as solutions and suspensions of inorganic salts.

Section 8 of this report contains detailed descriptions of 15 methods of water treatment that have been applied commercially to water streams that are similar or analogous to the streams from coal conversion plants. In the discussion that follows the applications of the methods are considered. The descriptions of the methods are omitted, to avoid repetition, except where they are required for clarification.

Oil-Water Separation by Gravity--
The API separator, tube settlers, and CPI separators all depend on the specific gravity difference between the oil and the water to effect separation. Effluents from these separators range from around 150 mg/l to 10 or 15 mg/l, depending on oil specific gravity, temperature and residence time. In refinery service the API separator has been thoroughly evaluated. The tube settler and the CPI separator appear to offer advantages in lower capital investment for separations comparable to the API separator.

Oil-Water Separation by Flocculation and Air Flotation--
May be used in combination with a gravity settler to reduce oils to the low levels of 10 to 15 mg/l that can be tolerated by biological oxidation. Such combinations usually reduce capital and operating costs below those of the gravity separator alone.

Boiler Feedwater Treatment--
The type and degree of treatment, and the treatment costs, depend on the raw water analysis and the analysis of the recycled water. A high solids content requires filtration with sludge disposal. A high dissolved solids content requires chemical precipitation that produces sludge. Demineralizers are required, particularly for high pressure boilers, and these produce a brine from

regeneration. According to the flowsheets developed for the Lurgi, Bigas and SRC II processes, recycled water to boiler feedwater treatment can range from 0 to about 50 percent of the total feedwater flow.

Phenol Recovery--
Lurgi's Phenosolvan process was investigated from the viewpoint of recovering for sale about 85 to 95 percent of the phenol available in the process quench condensate. The remainder of the phenol was considered to be destroyed in biological oxidation.

Phenol Destruction--
Anerobic digestion followed by aerobic digestion would consume all available phenol and allow elimination of the Phenosolvan process step. Wet air oxidation would also be effective, substituting for first stage biological oxidation, in destroying phenol.

Incineration--
May be a substitute for biological oxidation. Evaporation may be required. As an alternate, catalytic oxidation may be effective.

Biological Oxidation--
Usually considered as the final treatment step for wastewaters containing organics. Variations to increase activity, thus reducing retention time and capital and operating costs, include trickling filters, rotating biological contactors, fluidized sand beds, use of high purity oxygen activated sludge, nitrification and denitrification,and use of powdered activated carbon with wet oxidation regeneration.

Evaporation--
Multiple effect evaporation of streams bearing sludges from boiler feedwater treatment and cooling tower blowdown increases usable water recovery and decreases the quantity of salt-laden water to disposal, limited by salting out and scale formation on heat exchange surfaces to on the order of 11 percent solids. An alternate is the oil fluidized evaporator, which can yield dry solids. The total evaporator load may be lightened by use of reverse osmosis. The stream normally fed to biological oxidation may be evaporated.

Stripping--
Simple steam stripping is satisfactory when it is followed by biological oxidation. Without biological oxidation, as in the Bi-Gas process, lime treatment is also required. High chlorides in the water increase the problem.

Reverse Osmosis--
May be used with evaporation to reduce the evaporator load. Operation with inorganic and organic sludges is possible. May also be used to reject such inorganics as chlorides, sulfates, borates, silicates, phosphates, and nitrates from cooling tower makeup.

Ozonation, Activated Carbon, Alkaline Chlorination--
These methods may be required in Bi-Gas water treatment sequences to reduce ammonia, cyanides, and sulfides in water to be used for cooling tower makeup or boiler feedwater.

Selection of Processes for Economic Evaluation

In a coal conversion plant designed for maximum recycle of water, where the only water leaving the plant is contained in the solid waste and in cooling tower evaporation and drift, and where

contaminant removal to allow recycling has been demonstrated on waters similar or analogous to wastewaters from coal conversion plants, there are two areas to be investigated:

- Determination of the real similarities and differences between waters that have been effectively treated by commercial processes and wastewaters from conversion processes. This will permit decisions to be made on complete applicability of the control processes or only partial applicability that may require modification or further investigation

- Determination of the costs of the steps in the treatment sequence

Boiler Feedwater Treatment--
If the assumption is made that any wastewater that has been treated for recycling to the boiler feedwater system is no worse in quality than the raw water feed to the plant, then the boiler feedwater treating system is unaffected by changes in the other treatment steps. This assumption is recommended in the economic evaluation procedures; however, chemical precipitation followed by ion exchange should be compared with ion exchange alone and with reverse osmosis plus ion exchange.

Process Quench Condensate Treatment--
The treatment sequence shown in Figure 8-54 for Lurgi gasification includes oil-water separation, phenol extraction, stripping and ammonia recovery, air flotation, biological oxidation and sludge filtration. TABLE 8-62 shows the estimated costs for the several steps, and examination discloses that phenol extraction accounts for 34 percent of the total estimated capital, stripping/ammonia recovery 29 percent and biological oxidation/ sludge filtration 25 percent. Higher priority should thus be

placed on economic evaluation of these three steps since, among them, they account for 88 percent of the total. Economic evaluations of the process sequences could therefore be in the following order, with the provision that the final water stream to be recycled to the raw water system always has the same composition:

- Elimination of phenol extraction by adding anaerobic digestion to biological oxidation. In considering overall conversion plant economics, the reduction in revenue from elimination of phenol sales should be noted.

- Elimination of phenol extraction by substituting wet air oxidation for the first stages of biological oxidation

- Elimination of biological oxidation by feeding stripped water to the incinerator. Alternately, installation of an evaporator to recover water followed by incineration of evaporator bottoms may be evaluated. A second alternate is use of reverse osmosis instead of evaporation. In both alternates the sludge filter is eliminated

- In biological oxidation, contrast trickling filter, rotating biological contactors, fluidized sand beds, high purity oxygen activated sludge and powdered activated carbon with wet oxidation regeneration

Other economic evaluations for the remaining process sequence steps could be:

- Contrast API separators, tube settlers and CPI separators for oil-water separation

- Determine the effect on the air flotation step of changes in the separator step

Water Treatment Sludge and Cooling Tower Blowdown--
The sludges from boiler feedwater treatment and the cooling tower blowdown may be prepared for inclusion in the solid waste stream by evaporation, reverse osmosis, ion exchange or other means in various combinations. Economic evaluation should include:

- Evaporation of the total sludge plus blowdown stream to a solids content that avoids heat exchanger scaling. Evaluate costs versus number of effects

- Reverse osmosis followed by evaporation of the reject brine stream

- Reduce the cooling tower blowdown stream to evaporation by sidestream treatment by chemical precipitation, ion exchange or reverse osmosis, with sludge or reject brine going to evaporation

- Substitute oil-fluidized evaporation for conventional evaporation

- Eliminate water treatment sludge by using ion exchange in water treatment and feeding regeneration liquids to either type of evaporator

- The economics should be investigated for partial freezing of the water stream, separating the ice for recycle and evaporating the remaining liquid

TREATMENT OF GASEOUS EMISSIONS FROM COAL CONVERSION

Streams to be Treated

Boiler/Incinerator Offgas--
Sources of nitrogen oxides in offgas are nitrogen compounds in the coal, liquids, and gases to be incinerated and nitrogen in combustion air.

Source of particulates is entrained fly ash.

Sources of sulfur dioxide in offgas are sulfur compounds in coal and in liquids and gases to be incinerated.

Sulfur Recovery Offgas--
Source is the Claus or Stretford sulfur recovery unit. The quantity and composition are affected by the composition of the feed gas.

Cooling Tower Drift--
Source is the droplets of cooling tower water entrained in the cooling tower exhaust air.

Lock Hopper Vent Gas--
Source is residual gas in lock hoppers feeding coal to reactors.

Ash Quench Vent Gas--
Source is the ash quench pit at the reactor.

Storage Vessel Emissions--
Source is volatiles from tank breathing or filling.

Methods of Treatment

Particulates in boiler/incinerator offgases are removed by cyclones followed by wet scrubbers, wet scrubbers alone or cyclones followed by electrostatic precipitators.

Nitrogen oxides in boiler/incinerator offgas may be controlled by boiler modification, hydrotreating liquid fuels, and denitrification of flue gases.

Sulfur dioxide emissions from the incinerator/boiler may be reduced to meet present environmental standards by reducing the sulfur content in the feed coal physically, chemically or by a combination of both. Sulfur dioxide formation in the boiler may be reduced by fluidized bed combustion. Sulfur dioxide in the flue gases may be reduced by scrubbing to recover sulfur, scrubbing with discard of sulfur values or by dry absorption or reaction.

Hydrogen sulfide in the offgas from sulfur recovery may be reduced to meet present environmental standards by treatment to recover more sulfur or by incineration followed by the methods used for control of sulfur dioxide.

Cooling tower drift may be controlled by advanced design of mist eliminators in a forced draft tower by reducing air velocity in the tower or through use of natural draft tower designs.

Lock hopper vent gas may be controlled by releasing pressure through a compressor that returns the raw gas to the system, followed by a nitrogen or carbon dioxide purge, or by releasing the lock hopper gas to fuel gas or incineration followed by purging to fuel gas or incineration.

Ash quench vent gas may be controlled by separating the solids in a wet cyclone, condensing water vapor by direct contact with scrubber water and sending noncondensables to incineration.

Storage vessel emissions may be controlled by incineration, by refrigeration to condense the vapors, by scrubbing systems that use solvents of low volatility or by adsorption systems.

Selection of Processes for Evaluation

Control of nitrogen oxides in incinerator/boiler offgases appears to demand high priority in economic evaluation because of the possible, or probable, future reduction in allowable emissions. Economic evaluation should include the following:

- Reduction of emissions possible with boiler modifications. Cost of modifications. Separate evaluations for coal, waste tars, oils, and other liquids and waste gases. Evaluation for expected combinations of these

- The effect of feeding organic wastes in water suspension or solution on emissions, on boiler efficiency and on costs

- The hydrodenitrogenation of the waste tars and oils

- Denitrification of flue gases by wet and dry processes. Combination processes that also remove sulfur dioxide

Control of sulfur dioxide should include evaluations of:

- Processes for recovery of sulfur, sulfuric acid or concentrated sulfur dioxide from the boiler offgas. For processes, like the citrate process for sulfur recovery,

that use part of the hydrogen sulfide gas feed to the Claus or Stretford sulfur recovery unit as feed for conversion of sulfur dioxide, the effect on capital and operating costs of the Claus or Stretford unit should be evaluated

- Processes for desulfurization of flue gas by scrubbing with lime or limestone and discarding the resulting sludge. Evaluation of the overall effect on conversion plant economics of discarding part or all of the sulfur values in the coal feed

- Processes for simultaneously removing nitrogen and sulfur oxides from the boiler offgas

- Dry processes for sulfur dioxide removal, including direct injection of ammonia into the flue gas

- Processes for hydrodesulfurization of waste tar and oil. Combination hydrodesulfurization and hydrodenitrogenation

Control of particulates should be evaluated from the following viewpoints:

- If the incinerator/boiler offgases are to be treated dry for removal of gaseous pollutants, the particulate control should also be dry, as cyclones followed by electrostatic precipitators, hot gasifiers or baghouses

- If the offgases are to be treated wet, as in a recovery or throwaway scrubber system, cyclones to remove larger particulates may be the only control requirement

Control of hydrogen sulfide in Claus or Stetford sulfur recovery tail gas should be evaluated from these viewpoints:

- The economics of recovering more sulfur by adding tail gas treatment. Contrast Beavon, ARCO, SCOT and other promising recovery processes

- The economics of incinerating the offgas and recovering its sulfur values together with the sulfur values already in the incinerator/boiler offgas

- The economics of incinerating the offgas and removing the total sulfur values from the incinerator/boiler offgas by dry and by wet methods

Evaluation of control of cooling tower drift should include:

- Economics of replacing conventional drift eliminators with high efficiency types

- Economic comparison of forced draft cooling towers with high efficiency eliminators versus natural draft cooling towers

With regard to lock hopper vent gases, it is recommended that evaluation be limited to installation of a carbon dioxide or nitrogen purge system, with incineration of residual and purge gases.

Evaluation of controls for storage tank emissions may include the following:

- Economics of individual versus collective emissions treatment

- Economic comparision of incineration, refrigeration, scrubbing with recovery and adsorption with recovery

TREATMENT OF SOLID WASTES FROM COAL CONVERSION

Streams to be Treated

Fugitive Coal Dust--
Dusts are evolved during transit from coal mine to coal conversion plant, at the coal unloading station, during conveying and stacking in storage piles, during storage in piles, during reclaim and conveying to the coal preparation section of the conversion plant and in the milling and screening operations of coal preparation.

Solid Wastes--
This stream is principally ash or slag from gasifiers and utility boilers, but also includes inorganic salts in suspension or solution from water treating, spent catalysts, and other miscellaneous solid inorganic wastes. In this project no flue gas desulfurization sludge is considered to be generated.

Methods of Treatment

Fugitive Dusts in Transit--
Dust evolution may be suppressed by spraying a chemical binder on loaded cars before they leave the coal mine. Alternately, dust may be eliminated by separating all particles smaller than 500 micrometers in diameter, agglomerating them into particles 500 micrometers or larger in diameter, and combining the agglomerates with the main coal stream.

Fugitive Dusts at the Conversion Plant--
Dust evolution may be suppressed in coal unloading, handling, stacking and reclaiming to the coal preparation section by spraying a water solution of surfactant on the coal at various points in the system. Alternately, the incoming cars may be saturated with a water solution of surfactant prior to unloading.

Dust evolution from "dead" storage piles may be suppressed by application of a chemical binder

Dust evolution in coal preparation may be controlled by covering conveyors and screens and venting these and the mills to baghouses. Coal storage silos may be vented to dust collectors that return the dust to the silos.

Dust evolution in the conversion plant up to the screens and mills in coal preparation may be eliminated by separation and agglomeration of dust at the mine.

Solid Wastes--
In the disposal area the solid wastes may be deposited and compacted on an impervious membrane that isolates the wastes from ground and subsurface water.

The solids may be chemically stabilized before deposition in the disposal area. Depending on the permeability characteristics of the stabilized mass, an impervious membrane may, or may not, be interposed between the wastes and the soil.

Leachates--
To avoid accumulation of liquids in the solid waste disposal area, provision for bottom drainage of the area is required. Drainage may be through a pervious layer of sand and gravel

applied on top of the impervious membrane liner or as the bottom layer in the area prepared for chemically stabilized wastes. Alternately, drainage may be provided by pipes arranged in a drain field on the bottom of the disposal area.

Leachate should be conducted by lined ditches or pipes to a sump from which it may be pumped back to the conversion plant for use in ash quenching or for treatment and recycling into the conversion process.

Covering the Disposal Area--
The deposited and compacted solid wastes should be covered with at least two feet of soil, with the upper 6 inches being top soil, graded and sown with a ground cover.

Methods for Evaluation and Comparison of Control Processes

Economic evaluation of means of dust suppression should include the following:

- Estimation of the value of coal dust losses during transit, handling and storage to evaluate the incentive for suppressing dust

- Determination of capital and operating costs of spray systems to apply binders to cars at the mine, spray systems and any auxiliary systems needed to suppress and control dust evolution from moving coal streams in the conversion plant, spray systems for binders for "dead" storage piles.

Dust elimination methods should be contrasted with dust suppression methods in the following manner:

- Determine the capital and operating costs of dust control methods that are normally used at the mine in handling usable dust

- Determine capital and operating costs of the handling and drying system that is used for reclaiming wet coal fines

- Develop capital and operating costs for separation of dust from dry coal, including air elutriation and screening together with dust collection and storage

- Develop capital and operating costs for such methods of agglomerating coal dusts as compaction, briquetting and granulation together with costs of any associated processes or equipment

- Compare the total costs associated with dust agglomeration to the total costs associated with dust suppression

Capital and operating costs of solid waste disposal should be evaluated in the following manner:

- Evaluate such methods of solids transport as trucks, belt conveyors,and aerial tramways as means of moving solids from the conversion plant to the disposal area

- Determine costs of preparation of the disposal area, including the drainage and return system and the cover. Consider level ground, strip mines,and valleys

- Determine costs of installation of impervious liners. Evaluate liners according to durability in service and cost

- Evaluate chemical stabilization systems according to system capital and operating cost, such associated costs as slurry pumping, supernatant water return, need for an impervious liner during or after filling of the area and need for special treatment of the stabilized mass. Consider the IUCS, Dravo and Chemfix systems, together with any other promising systems

BASIS FOR ECONOMIC STUDIES

Composition of Raw Water

To evaluate the effect of variation in raw water analysis on the boiler feedwater treatment costs, it is suggested that the effect of, say, 6 analyses drawn from various areas of the U.S. be evaluated for one water treatment sequence, that factors be calculated for the effect of changing analysis on capital and operating costs for that treatment process, that one water anyalsis be evaluated in the other treating processes and that the multiplying factors be applied to the other processes to demonstrate the economic effect of changing processes and changing analyses.

Coal Feed Analysis

It is suggested that coal feeds be chosen as low sulfur western coal, high sulfur eastern coal and lignite.

Conversion Process Effluent Emission and Waste Compositions and Quantities

It is suggested that the data and information on these streams that were developed for this project be updated and amplified

with real data from actual operations of the conversion processes wherever possible. When analyses are lacking, best engineering estimates are suggested as a working basis.

Capital Cost Data

Costs supplied by treatment process licensors, equipment vendors, or others should be carefully examined by a cost estimating expert to ascertain that assembly of final installed costs of equipment includes all of the engineering, procurement, and construction costs.

Plot Plans

These may be required for estimation of piping, electrical, and other costs.

Operating Cost Development

Chemical usage and utilities requirements should be stated by the process or equipment suppliers. Manpower and maintenance costs should be developed by a skilled estimator.

Location Adjustments

Variations in costs for construction labor and materials for selected U. S. locations should be developed as factors by the cost estimator to be applied as multipliers to the costs developed for a (selected) base case loction, such as the U. S. Gulf Coast.

Capacity Adjustments

Multiplying factors for application to a (selected) base case capacity should be developed by the cost estimator.

Cost Basis and Updating Factors

The cost basis should be established for a convenient year quarter and be firmly adhered to. Updatings to later bases can be made by use of an overall multiplier, such as an inflation factor or, in the case of capital costs, by cost change multipliers derived from categories of equipment or services or from representative requotations of equipment.

THE CAPITAL COST MODEL

E = Major Equipment. This is the delivered material cost of equipment and includes furnaces, heat exchangers, converters, reactors, towers, drums and tanks, pumps, compressors, transportation and conveying equipment, special equipment (filters, centrifuges, dryers, agitators, grinding equipment, cyclones, etc.), and major gas ductwork.

M = Other Material Costs. This includes the cost of piping, electrical, process instrumentation, paint, insulation, foundations, concrete structures, and structural steel for equipment support. It also includes such items as site preparation and steel frame structures and may include process buildings and control rooms. Shops and offices, though they may be necessary, are usually considered as offsite items.

L = Field Construction Costs. This includes the cost of direct field construction labor, fringe benefits and payroll burden, field administration, supervision and temporary facilities, construction equipment and tools.

H = Home Office Engineering Costs. This includes home office construction, engineering and design, procurement, client

services, accounting, cost engineering, travel and living expenses, reproduction, and communication.

B = Base Cost of the Installed Process. This is defined as the sum of equipment costs, other material costs, construction labor and labor indirects, and home office engineering. For the base case location, B = E + M + L + H.

TI = Taxes and Insurance. These are costs incurred during the construction period.

OP = Overhead and Profit. This is a cost charged to the project by the contractor.

C = Contingency. Usually expressed as a fraction of B, the base cost of the plant, it represents the degree of uncertainty in the process design and the cost estimate. It may range from 0.0 to 0.1 for a well-established process whose costs are well documented. It may range to 0.2 or more for a process that is still under development, where capacity, location or other parameters have changed from the base case or where costs were not well documented and factors for M, L, and H must be used instead of real figures.

TPI = Total Process Investment. This is defined as the sum of the bare cost (including contingency), taxes and insurance, and contractor's overhead and profit:

$$TPI = E + M + L + H + TI + OP + C$$

S = Startup Costs. These costs include commissioning the installed process, installing catalysts and chemicals and, in general, readying the installation for onstream operation.

W = Working Capital. This capital is required for such items as raw materials inventory and materials and supplies for the process.

IC = Interest During Construction. This cost depends on the duration of the construction period, from signing of the construction contract to "ready for commissioning."

TCR = Total Capital Required. This is the sum of all the above items:

$$TCR = E + M + L + H + TI + OP + C + S + W + IC$$

THE OPERATING COST MODEL

R = Annual Cost of Raw Materials, Utilities and Waste Disposal. Byproduct credit should be substracted from this cost.

OL = Annual Cost of Operating Labor. Includes cost of operating labor supervision.

ML = Annual Cost of Maintenance Labor. Includes cost of maintenance labor supervision.

PS = Annual Cost of Process Supplies. This may include charts, cleaning supplies, miscellaneous chemicals, lubricants, paint and replacement parts such as gaskets, seals, valves, insulation, welding materials, packing, and vessel lining materials.

OH = Annual Cost of Administration and Overheads. These costs include salaries and wages for administrators, secretaries, typists and clerks and such other costs as office supplies and equipment, medical and safety services, transportation and

communications, lighting, janitorial services, plant protection, payroll overheads and employee benefits.

AT = Annual Local Taxes and Insurance. Included are property taxes, fire and liability insurance and other items such as special hazards insurance and business interruption insurance.

AOC = Total Net Annual Operating Cost. This is the sum of the operating costs items:

$$ACO = R + OF + ML + PS + OH + AT$$

D = Annual Depreciation. This may be calculated by the straight-line method, where TCR - W is divided by the expected life of the process. Other methods may be used, such as declining balance and sum-of-the-digits.

IR = Average Annual Interest on Borrowed Capital + Average Annual Net Return on Equity. These are calculated according to a procedure recommended in the literature.* The procedure assumes a fixed debt-to-equity ratio, an interest rate on debt, and the required net (after tax) rate of return on equity. Interest on debt and return on equity are calculated over the plant life, and the yearly average is expressed as a percentage of the total capital required (TCR).

FT = Federal Income Tax. This is the average yearly income tax over the process life, expressed as a percentage of the total capital required (TCR).

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*Synthetic Gas-Coal Task Force, "Final report - The Supply-Technical Advisory Task Force - Synthetic Gas-Coal," prepared for the Supply-Technical Advisory Committee, National Gas Survey, Federal Power Comission, April 1973.

APC = Total Annual Production Cost. This is the sum of the above items:

$$APC = AOC + D + IR + FT$$

USE OF THE COST MODELS

The general cost model that has been described will provide a standard format for estimating process economics so that economic comparisions between processes may be made on a consistent basis by ensuring that all estimates include the same cost items.

This general cost model uses a utility-type financing method and is based on a procedure recommended in the literature.* Fundamentally, the model assumes no time value for money. That is, for estimating the economics of control processes, such items as interest on debt and return on investment can be related to capital costs by simple percentages which remain constant from year to year. This method allows a simple, straight-forward calculation of process operating costs.

(It should be noted that the discounted cash flow method may also be used to determine capital and operating costs for the processes. This method, because it takes into account the time value of money, may more nearly apply to industrial operations than does the utility financing method. The discounted cash flow method is based on the same literature reference as the previous method.*)

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*Synthetic Gas-Coal Task Force, "Final Report - The Supply-Technical Advisory Task Force - Synthetic Gas-Coal," prepared for the Supply-Technical Advisory Committee, National Gas Survey, Federal Power Commission, April, 1973.

SECTION 12

TECHNOLOGY TRANSFER

REPORTS COMPLETED

The draft report "Environmental Standards Applicable to Coal Conversion Processes" by Donald K. Webber and Donald E. Whittaker was delivered to EPA in September 1978.

ABSTRACT

Existing and proposed environmental standards have been gathered and synopsized to serve as a guide for evaluation of the efficiency of available and developing technology for control of liquid effluents, gaseous emissions, and solid wastes from coal conversion processes. Within the United States, the Federal and EPA standards and guidelines for air, water, and solid wastes were gathered, together with the standards for 22 states selected for their potential in installation of coal conversion facilities and the standard for two regional commissions. With a view toward the possibility of environmental effects crossing national borders, the standards and guidelines for Mexico, the Dominion of Canada, two Canadian provinces and the International Joint Commission of U.S. and Canada, were synopsized and added to the U.S. standards.

All of the standards and guidelines were compared and from them a summary of the most stringent of the standards was developed. This summarization, reduced as far as possible to engineering terms, can serve as a guide in the design of coal conversion plants on the premise that if the effluents, emissions,and wastes from the conversion process steps are so treated that the final releases to the environment meet the criteria in the summary of most stringent standards, then the conversion plants can be built anywhere in the U.S., Mexico,or Canada.

SYMPOSIA AND MEETINGS

At a contractors' symposium at RTP in June 1977 the Pullman Kellogg program was discussed and areas in which the program overlapped, supplemented or was supplemented by other programs in progress were defined.

At the Florida EPA symposium in September 1977, " Environmental Aspects of Fuel Conversion Technology, III," the paper "Control Technology Development for Fuel Conversion Wastes" was presented:

ABSTRACT

Pullman Kellogg's contract with the Environmental Protection Agency concerns control technology development for fuel conversion system waste utilization and disposal, for coal storage, preparation and feeding and for wastewater treatment. The program includes assessment of available and developing control technology as applied to fuel conversion effluents/emissions/wastes and relationship to present and proposed environmental regulations, continues with theoretical and experimental development of promising alternate control technologies, then concludes with an overall comparative analysis of all technologies and an

engineering design and cost estimate for those control methods judged to be appropriate for integration into conversion system flow schemes.

Since the program has been operating for only five of its scheduled 36 months, this paper may be considered as a progress and planning report.

A paper "Environmental Program of Solid Wastes from Synthetic Fuels from Coal Technologies" was prepared for presentation at the November 1977 meeting of AIChE in New York:

ABSTRACT

Pullman Kellogg's contract with EPA reflects the concepts of the synfuels program in its title: "Control Technology Development for Fuel Conversion System Waste Utilization and Disposal; Coal Storage, Preparation and Feeding; and Wastewater Treatment." The work is divided into assessment of available and developing control technology, control technology development and control technology evaluation. The desired end product of the effort is the development of control technology in the areas of conversion system wastes, coal processing as applied to coal conversion systems and water management. The work is designed to interface with other studies in the EPA synfuels program for interchange of information and definition of problems. These studies include physical and chemical coal cleaning, control technology for fuel converter output streams and the products and byproducts of fuel conversion systems, and environmental assessments in gasification and liquefaction. Although the contract includes aspects of control technology for solid, liquid, and gaseous emissions from fuel conversion process, and Kellogg's efforts are directed into all three areas, only solid wastes will be considered in the discussion that follows.

APPENDIX

PROJECT BIBLIOGRAPHY: PULLMAN KELLOGG REFERENCE FILE

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APPENDIX

PROJECT BIBLIOGRAPHY: PULLMAN KELLOGG REFERENCE FILE

The project bibliography was modeled on the Pullman Kellogg Information and Retrieval (ISTAR) system that was developed in the Research and Development Center. The indexes were established to provide easy identification, access and retrieval of the many documents that were obtained for the project.

The indexes provide identification of the content of the documents. They do not provide abstracts or other in-depth access to the subject matter, since detailed retrieval of information can be accomplished through use of such commercial data services as NTIS and Chemical Abstracts.

Documents bearing accession numbers up to and including 252 were gathered by Pullman Kellogg prior to the beginning of the project. These documents are the property of Pullman Kellogg. Documents bearing accession numbers 253 and subsequent were purchased with funds from this project and are therefore Government property.

Subject List

A standarized subject list of keywords, TABLE A-1, was developed to describe the principal concepts in each document. Each document, upon receipt, was assigned a unique accession number to

identify its position in the filing system. Then, from the subject list, each document was assigned from 1 to 5 keywords to identify the subject matter.

The abbreviation "S.A." denotes "See Also" and guides the user to related terms.

TABLE A-1. SUBJECT LIST

ACETYLENE
ACTIVATED CARBON --------SEE CARBON
ACTIVATED SLUDGE --------SEE SLUDGE
ADSORPTION
AMMONIA
ANALYSIS
ASH ----------S.A. COAL ASH
ASPHALT
BIBLIOGRAPHY
BIGAS
BIOX ----------BIOLOGICAL OXIDATION
BOD ----------BIOLOGICAL OXYGEN DEMAND
BOILER
BUR. OF MINES
CARBON
CARBON DIOXIDE
CARBONIZATION
CARBONYLS
CATALYST
CHAR OIL
CHLORINE
CITRATE PROCESS
CLAUS GAS
CLEAN COKE
CO(2) ACCEPTOR
COAGULATION
COAL ----------S.A. LIGNITE, PYRITE
COAL ASH ----------SEE ASH
COAL CHAR
COAL CLEANING ----------S.A. FILTRATION
COAL COMBUSTION

TABLE A-1. SUBJECT LIST (CONT)

COAL CONVERSION --------S.A. SPECIFIC PROCESSES
COAL GASIFICATION --------S.A. SPECIFIC PROCESSES
COAL HANDLING
COAL LIQUEFACTION --------S.A. SPECIFIC PROCESSES
COAL MINING
COAL PLANT
COALCON
COED
COG REFINERY ----------COAL-OIL-GAS REFINERY
COGAS
COKING
CONSOL
CORROSION
CRUDE OIL
CYANIDES
DESALINATION
DESULFN. ----------S.A. SULFUR, EMISSIONS, SCRUBBING
DONOR SOLVENT
DRAVO
EFFLUENTS ----------S.A. EMISSIONS, WASTEWATER, POLLUTION
EMISSIONS ----------S.A. POLLUTION, DESULFN., SCRUBBING
ENERGY
ENTRAINMENT
ENVIRONMENT ----------S.A. POLLUTION
EPA
ERDA
FBC ----------FLUID BED COMBUSTOR, S.A. COAL COMBUSTION
FILTRATION ----------S.A. COAL CLEANING
FLOCCULATION
FLOTATION
FLUID BED ----------S.A. FBC

TABLE A-1. SUBJECT LIST (CONT)

FLUORIDES
FUEL ----------S.A. SOLID, LIQUID OR GASEOUS FUEL
FUEL CELL
FUEL GAS
FUEL OIL
GAS
GASEOUS FUEL
GASOLINE
H-COAL
HEALTH ----------S.A. SAFETY, TOXICITY
HEAT EXCHANGER
HYDRODESULFN----------HYDRODESULFURIZATION
HYDROGASIFICATION -----S.A. HYGAS
HYDROGEN
HYDROGEN SULFIDE
HYDROGENATION
HYDROTREATING
HYGAS ----------S.A. HYDROGASIFICATION, IGT
IGT ----------S.A. HYGAS, HYDROGASIFICATION
KINETICS
KOPPERS
LEACHING ----------S.A. SOLID WASTE
LIGNITE ----------S.A. COAL, PYRITE
LIQUID FUEL
LNG ----------LIQUID NATURAL GAS
LURGI
MEMBRANE
METAL ----------S.A. TRACE ELEMENTS
METHANATION
METHANE
METHANOL

TABLE A-1. SUBJECT LIST (CONT)

MEYERS
MOLTEN SALT
NATURAL GAS
NITROGEN OXIDES ----------S.A. EMISSIONS, POLLUTION
OIL ----------S.A. CRUDE OIL, FUEL OIL
OIL SHALE
OXYGEN
OZONE
PARAHO
PEDCO
PHENOL
PIPELINE GAS ----------SEE FUEL GAS
PNA ----------POLYNUCLEAR AROMATICS
POLLUTION ----------S.A. ENVIRONMENT, HEALTH, WASTE
POWER CYCLE
POWER PLANT
PYRITE ----------S.A. COAL, LIGNITE
PYROLYSIS
REGENERATION
REGULATIONS ----------S.A. STANDARDS
SAFETY ----------S.A. HEALTH, TOXICITY
SCRUBBER
SCRUBBING
SEPARATION ----------S.A. ANALYSIS
SLUDGE
SLURRY
SNG ----------SYNTHETIC NATURAL GAS
SOLID FUEL
SOUR WATER
SRC ----------SOLVENT REFINED COAL

TABLE A-1. SUBJECT LIST (CONT)

STANDARDS ----------S.A. REGULATIONS
STEEL
SULFUR ----------S.A. DESULFN.
SULFUR DIOXIDE ---------S.A. DESULFN., SCRUBBING, EMISSIONS
SYNTHANE
SYNTHOIL
TAR
TAR SANDS
THICKENERS
TOWER
TOXICITY ----------S.A. HEALTH, SAFETY
TRACE ELEMENTS
TRW
TVA ----------TENNESSEE VALLEY AUTHORITY
UGAS
WASTE ----------S.A. POLLUTION, EMISSIONS, EFFLUENTS
WASTEWATER ----------S.A. WATER, POLLUTION, EFFLENTS
WATER ----------S.A. WASTEWATER
WESTINGHOUSE
WINKLER

Bibliography Index

The bibliography index is arranged in order by accession number. The index contains all the bibliographic information for each document in a fixed format. Following is the content of each line of the format:

Line Identification	
10 and 11	Title
20 and 21	Source (journal, conference) or subtitle
30	Personal authors (up to 5)
31	Corporate author
40	Organization for which work was done (or publisher), their report number and NTIS order number

An "X" at the end of the title indicates that the bibliographic information may be incomplete.

Keyword Index

Each document can have from 1 to 5 lines of keywords to describe it. The first word of each line must come from the subject list. Then, any other keywords that describe the particular document can be added to that line.

Since most of the documents dealt with coal conversion, general terms such as "Coal Gasification" or "Coal Liquefaction" were only to describe reports that dealt with many different processes.

A report on 1 or 2 specific processes would be indexed under those specific processes and not under a general term. For example, a report on Lurgi coal gasification would be indexed under "Lurgi," while a symposium on coal gasification would be indexed under "Coal Gasification," even though the Lurgi process would be mentioned in the symposium. This method of selection of keywords applies throughout the index to other general terms, such as emissions or wastewater.

Other pertinent information, such as the personal author, the file code number (01 for this file), the accession number and the type of document are also included in this index. TABLE A-2 lists the types of documents and their codes. More information on the document can then be found by using the accession number to refer to the bibliography index.

Title Index

The title index is an alphabetical list of the first lines of the titles of all the documents. When "a", "an", or "the" was the first word of the title, it was omitted. The title index refers the user to the accession number, which can be used to find further information in the bibliography index.

Author Index

The names of authors are inverted and only one intial is used, i.e., Smith, J. The maximum number of authors indexed for each document is the same as the number of lines of keywords that are used. For example, a document with only two lines of keywords that has five authors will have only the first two authors listed

TABLE A-2. DOCUMENT CODES

CODE	TYPE OF DOCUMENT
A	Minutes of Meetings
B	Bibliography
C	Contracts
D	Invention Disclosures
E	Articles or Papers
F	Flowsheets
G	Correspondence with Outside
H	Outside Reports
I	Patents
J	Books
L	Legal Documents
M	Monthly Reports
P	Proposals
R	Kellogg Research Reports
T	Kellogg Miscellaneous Reports
(blank)	Internal Memos

in the author index. However, all five authors for the same document can be found in the bibliography index. When there are fewer authors than the number of lines of keywords, the authors' names are repeated to equal the number of lines of keywords.

Corporate Author Index

The organization which generated the report is listed in this index. When there was more than one organization involved, only the organization of the first personal author is included. Abbreviations that are used for some of the organizations are shown in TABLE A-3.

Report Number Index

This index lists the report numbers as given by the issuing agency. For example an EPA report would be listed as E600 2-75-014 and an ERDA report as FE 237156.

NTIS Order Number Index

This index lists the number assigned by NTIS. This index, and the previous one, were used primarily for ordering information.

TABLE A-3. LIST OF ABBREVIATIONS OF ORGANIZATIONS

ACS	AMERICAN CHEMICAL SOCIETY
AGA	AMERICAN GAS ASSOCIATION
AICHE	AMERICAN INSTITUTE OF CHEMICAL ENGINEERS
AIME	AMERICAN INSTITUTE OF MINING ENGINEERS
API	AMERICAN PETROLEUM INSTITUTE
AWARE	ASSOCIATED WATER & AIR RESOURCES ENGINEERS, INC.
BCR	BITUMINOUS COAL RESEARCH
BNL	BROOKHAVEN NATIONAL LABORATORY
BOR	BUREAU OF RECLAMATION
CCC	CONSOLIDATED COAL CO.
CCNA	CHEMISTRY CONGRESS OF NORTH AMERICA
CEQ	COUNCIL ON ENVIRONMENTAL QUALITY
DBER	DIVISION OF BIOMEDICAL & ENVIRONMENTAL RESEARCH
EESD	ENERGY & ENVIRONMENTAL SYSTEMS DIVISION
EMSL	ENVIRONMENTAL MONITORING & SUPPORT LABORATORY
EPA	ENVIRONMENTAL PROTECTION AGENCY
EPRI	ELECTRIC POWER RESEARCH INSTITUTE
ERDA	ENERGY RESEARCH AND DEVELOPMENT ADMINISTRATION
ERL	ENVIRONMENTAL RESEARCH LABORATORY
ESOWP	ENGINEERS SOCIETY OF WESTERN PENNSYLVANIA
FPC	FEDERAL POWER COMMISSION
GWDA	GULF WASTE DISPOSAL AUTHORITY
IECEC	INTERSOCIETY ENERGY CONSERVATION ENGINEERING CONF.
IERL	INDUSTRIAL AND ENGINEERING RESEARCH LABORATORY
IIEQ	ILLINOIS INSTITUTE OF ENVIRONMENTAL QUALITY
IGT	INSTITUTE OF GAS TECHNOLOGY
IMMR	INSTITUTE FOR MINING AND MINERAL RESEARCH
LERC	LARAMIE ENERGY RESEARCH CENTER
MERC	MORGANTOWN ENERGY RESEARCH CENTER
MERL	MUNICIPAL ENVIRONMENTAL RESEARCH LABORATORY
MIT	MASSACHUSETTS INSTITUTE OF TECHNOLOGY

TABLE A-3. LIST OF ABBREVIATIONS OF ORGANIZATIONS (CONT)

NAPCA	NATIONAL AIR POLLUTION CONTROL ADMINISTRATION
NCA	NATIONAL COAL ASSOCIATION
NCWQ	NATIONAL COMMISSION ON WATER QUALITY
NERC	NATIONAL ENVIRONMENTAL RESEARCH CENTER
NIOSH	NATIONAL INSTITUTE FOR OCCUPATIONAL SAFETY & HEALTH
NSF	NATIONAL SCIENCE FOUNDATION
NTIS	NATIONAL TECHNICAL INFORMATION CENTER
OEMI	OFFICE OF ENERGY, MINERALS, & INDUSTRY
OFF. OF WRT	OFFICE OF WATER, RESEARCH AND TECHNOLOGY
OFFICE OF AQPS	OFFICE OF AIR QUALITY PLANNING & STANDARDS
ORNL	OAK RIDGE NATIONAL LABORATORY
OWHM	OFFICE OF WATER & HAZARDOUS MATERIALS
PERC	PITTSBURGH ENERGY RESEARCH CENTER
PIWC	PURDUE INDUSTRIAL WASTE CONFERENCE
TIC	TECHNICAL INFORMATION CENTER
TWQB	TEXAS WATER QUALITY BOARD
USDA	U.S. DEPARTMENT OF AGRICULTURE
USDI	U.S. DEPARTMENT OF THE INTERIOR
USDOE	U.S. DEPARTMENT OF ENERGY
USGS	U.S. GEOLOGICAL SURVEY
USNRC	U.S. NUCLEAR REGULATORY COMMISSION
VNR	VAN NOSTRAND REINHOLD CO.
WPCF	WATER POLLUTION CONTROL FEDERATION

PULLMAN KELLOGG INFORMATION STORAGE AND RETRIEVAL SYSTEM
RESEARCH INFORMATION DIVISION
FILE---01 EPA 68-02-2198 FUEL CONVERSION DATE---SEPTEMBER 1979
INFORMATION ARRANGED BY AUTHOR PAGE--- 1

AUTHOR	SUBJECT	ACCESSION NUMBER	TYPE OF DOCUMENT
ABEL, W.	COAL CLEANING, PYRITE, SEPARATION, BUR. OF MINES	01 0415	H
ADAMS, A.	CARBON, POWDERED, ACTIVATED SLUDGE IMPROVEMENT	01 0928	E
ADAMS, C.	SLUDGE, REFINERY, HANDLING, SOURCES	01 0828	E
ADAMS, C.	BOD, WASTEWATER PRETREATMENT, ECONOMICS	01 0858	E
ADAMS, C.	PHENOL, WASTE TREATMENT, ACTIVATED SLUDGE	01 0963	E
ADAMS, C.	COKE, PLANT WASTEWATER, TREATMENT, EPA GUIDELINES	01 0967	E
AL-HAJ-ALI, N.	EMISSIONS, SO(2) CONTROL, DESULFN.	01 0732	H
ALEXANDER, W.	SRC, LIQUID FUEL, CHARACTERIZATION, HANDLING	01 0274	B
ALFORD, A.	ANALYSIS, MS-GC, WASTEWATER	01 0391	H
ALLEN, C.	FUEL GAS, SULFUR, REMOVAL	01 0270	H
ALPERT, S.	COAL GASIFICATION, HYDROGENATION, OXYGEN	01 0066	E
ANDERSON, L.	WASTE, ORGANIC, CONVERSION TO FUEL + ENERGY	01 0009	H
ANDERSON, W.	LEACHING, COAL PILE, CHARACTERISTICS	01 0922	E
ANDREWS, J.	SULFUR, EMISSIONS CONTROL, CLAUS PLANT	01 0576	E
ANTONIE, R.	WASTEWATER, TREATMENT, FIXED BIOLOGICAL SURFACES	01 0789	J
ARCHERD, F.	CARBON, ACTIVATED, ADSORPTION, WASTEWATER	01 0647	H
ARCHERD, F.	PHENOL, REMOVAL, WASTEWATER, ACTIVATED CARBON	01 0649	H
ARELLA, D.	WASTE, SOLID, METAL RECOVERY, INCINERATOR RESIDUE	01 0533	H

PULLMAN KELLOGG INFORMATION STORAGE AND RETRIEVAL SYSTEM
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INFORMATION ARRANGED BY AUTHOR PAGE--- 2

AUTHOR	SUBJECT	ACCESSION NUMBER	TYPE OF DOCUMENT
ARMSTRONG, T.	WASTEWATER, TREATMENT, HYDROGEN PLANT, CHEVRON PROCESS	01 0964	E
ARNOLD, T.	CONSTRUCTION, COST INDEXES	01 0888	E
ARORA, J.	FUEL GAS, HYDROGASIFICATION, ELECTROTHERMAL, LIGNITE	01 0164	H
ATKINS, W.	EFFLUENTS, TREATMENT, AMMONIA SEPARATION, PROCESS COMPAR.	01 0823	H
ATTARI, A.	COAL GASIFICATION, TRACE ELEMENTS, ENVIRONMENT	01 0322	H
ATTARI, A.	TRACE ELEMENTS, FATE, COAL GASIFICATION	01 0395	H
ATTARI, A.	IGT, TRACE ELEMENTS, DISTN. IN PROCESS STREAMS	01 0479	E
ATTARI, A.	TRACE ELEMENTS, COAL GASIFICATION, HYGAS	01 0673	H
ATWOOD, M.	TAR SANDS, OIL SHALE	01 0516	E
AUL	DESULFN., FLUE GAS, REGENERABLE PROCESS, FINAL REPORT,V.1	01 0627	H
AUL	DESULFN., FLUE GAS, REGENERABLE PROCESS, FINAL REPORT,V.2	01 0644	H
AYER, F.	ENVIRONMENT, FUEL CONVERSION PROCESSES, TRACE ELEMENTS	01 0036	H
AYER, F.	ENVIRONMENT, FUEL CONVERSION, SYMPOSIUM	01 0230	E
BABU, S.	COAL GASIFICATION, FLUID BED	01 0339	E
BACKER, R.	WASTE, SLUDGE, PHYSICAL PROP., WESTERN COAL	01 0600	H
BACKER, R.	WASTE, EMBANKMENT, PHYSICAL PROP., COAL MINING	01 0766	H
BAILIN, L.	WASTE, HAZARDOUS DETOXIFICATION, MICROWAVE PLASMA	01 0713	H
BAIR, W.	HYGAS, ASH, AGGLUMERATION, COAL CHAR, GASIFICATION	01 0337	E

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RESEARCH INFORMATION DIVISION
FILE---01 EPA 68-02-2198 FUEL CONVERSION DATE---SEPTEMBER 1979
INFORMATION ARRANGED BY AUTHOR PAGE--- 3

AUTHOR	SUBJECT	ACCESSION NUMBER	TYPE OF DOCUMENT
BAKER, A.	PYRITE, TWO-STAGE FROTH PROCESS, FLOTATION	01 0374	E
BALL, D.	ENVIRONMENT, LOW-BTU GAS, RETROFITTING INDUSTRIES	01 0257	H
BARKER, J.	BIOX, CARBON + NITROGEN REMOVAL, COKE PLANT WASTES	01 0800	H
BARRIER, J.	DESULFN., SLUDGE, DISPOSAL, ECONOMICS	01 0751	E
BARRY, C.	SULFUR, EMISSION REDUCTION, CLAUS PLANT	01 0568	E
BARTHEL, Y.	CLAUS GAS, TREATMENT	01 0559	E
BAUMANN, E.	FILTRATION, DESIGN CONSIDERATIONS, WASTEWATER	01 0496	H
BEARD, S.	COAL GASIFICATION, UNDERGROUND, THERMOCOUPLES	01 0473	H
BEARSE, A.	COAL, OXIDATION, CHEMICALS PRODN.	01 0152	H
BEAVON, D.	DESULFN., BEAVON PROCESS	01 0905	E
BECK, G.	WASTEWATER, TREATMENT, INSTRUMENTATION, PHILADELPHIA ELEC.	01 0920	E
BECKER, D.	EFFLUENTS, ENTRAINMENT, COAL GASIFICATION, FUEL GAS	01 0469	H
BEESON, J.	COAL CHAR, GASIFICATION, ELECTROFLUID REACTOR	01 0158	E
BENDORAITIS, J.	H-COAL, SRC, SYNTHOIL, LIQUID FUEL, COAL LIQUIDS	01 0251	H
BENNETT, G.	WASTEWATER, TREATMENT, POWER PLANT, ACTIVATED CARBON	01 0518	E
BERRY, W.	SOUR WATER, STRIPPER, CORROSION, VARIABLES	01 0968	H

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FILE---01 EPA 68-02-2198 FUEL CONVERSION DATE---SEPTEMBER 1979
INFORMATION ARRANGED BY AUTHOR PAGE--- 4

AUTHOR	SUBJECT	ACCESSION NUMBER	TYPE OF DOCUMENT
BERTOLACINI,R.	CATALYST, DEVELOPMENT, COAL LIQUEFACTION	01 0255	H
BERTRAND, R.	COAL GASIFICATION, ENVIRONMENT	01 0903	E
BERUBE, D.	DESULFN., FLUE GAS, MONTANA POWER CO., EVALN.	01 0752	E
BEYCHOK, M.	LIQUID FUEL, SNG, LNG, PROCESS	01 0702	H
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GARDNER, F.	CARBON, ACTIVATED, WASTEWATER, PURIFICATION	01 0530	H
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GASIOR, S.	EFFLUENTS, TAR, CHAR, GAS,SYNTHANE,ANALYSIS,BUR. OF MINES	01 0406	H
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GLOVER, T.	COAL HANDLING, UNIT TRAIN TRANSPORTATION, BUR. OF MINES	01 0418	H
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SHARKEY, A.	ANALYSIS, COAL GASIFICATION, SYNTHANE, WASTEWATER	01 0356	H
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SMITH, J.	WASTEWATER, RESIDUALS MANAGEMENT, CONFERENCE, SLUDGE	01 0324	H
SMITH, J.	OIL SHALE, TAR SANDS	01 0516	E
SMITH, M.	COAL MINING, WASTE DISPOSAL, ENVIRONMENT	01 0316	B
SMITH, M.	ASH, FLY, BIBLIOGRAPHY, 1975-1977	01 0791	B

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SMITH, M.	ASH, FLY ASH, BIBLIOGRAPHY, 1976-1977	01 0824	B
SMITHSON, G.	EMISSIONS, HAZARDOUS, COKING, HEALTH, SRC, LURGI	01 0037	H
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01 0001	PARSONS, RALPH M., CO.
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ENVIRONMENT, TRACE ELEMENTS, SLUDGE, ASH	LOWELL, P.	01 0410	H
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EPA, WASTE, SOLID, SLUDGE, ANAEROBIC DIGESTION, METHANE	RITTE, S.	01 0491	H
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ERDA, EFFLUENTS, GAS & LIQUID, CONTROL, HOE CREEK, IN SITU	MEAD, W.	01 0402	H
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FBC, AIR POLLUTION CONTROL, AICHE SYMPOSIUM	WEINSTEIN, N.	01 0902	E
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FBC, ELECTRIC UTILITY LARGE STEAM GENERATORS	DOWDY, T.	01 0773	H
FBC, EMISSIONS, WASTE, SOLID, EPA PROGRAM		01 0532	H
FBC, ERDA QUARTERLY REPORT, COAL COMBUSTION		01 0571	H
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FILTRATION, DESIGN CONSIDERATIONS, WASTEWATER	BAUMANN, E.	01 0496	H
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FILTRATION, GRAVITY SETTLERS, SAMPLING, WASTE, COAL		01 0668	H
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FLUID BED, COAL GASIFICATION	SHAH, B.	01 0339	E
FLUID BED, COAL GASIFICATION, DESIGN, WESTINGHOUSE	LEMEZIS, S.	01 0378	H
FLUID BED, MECHANICS, CO(2) ACCEPTOR	GORIN, E.	01 0127	H
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FUEL GAS, PRODN., HYDROGASIFICATION, BITUMINOUS COAL	KNABEL, S.	01 0193	H
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GASEOUS FUEL, FROM WASTE, LIQUID FUEL	LEHMANN, E.	01 0470	B
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GASOLINE, CATALYST, ZINC CHLORIDE, HYDROCRACKING		01 0120	H
GASOLINE, COAL CLEANING, HYDROCRACKING, CONSOL		01 0118	H
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H-COAL, ENERGY RESEARCH PANEL		01 0062	E
H-COAL, INTEGRATED PP LAB STUDY		01 0277	H
H-COAL, INTEGRATED PP, HYDROCARBON RESEARCH, FINAL REPORT		01 0811	H
H-COAL, KENTUCKY PP		01 0073	E
H-COAL, LIQUID FUEL, ECONOMICS		01 0507	H
H-COAL, POLLUTION CONTROL, EVALN.	JAHNIG, C.	01 0219	H
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H-COAL, SRC, SYNTHOIL, LIQUID FUEL, COAL LIQUIDS	BENDORAITIS, J.	01 0251	H
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H-COAL, WASTEWATER TREATMENT	DAVIS, G.	01 0678	H
H-COAL, WASTEWATER, TREATMENT	REAP, E.	01 0654	H
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HYDROGASIFICATION, BITUMINOUS COAL, FUEL GAS PRODN.	TSAROS, C.	01	0193	H
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LIQUID FUEL, COAL LIQUIDS, H-COAL, SRC, SYNTHOIL	STEIN, T.	01 0251	H
LIQUID FUEL, CONSOL PP, DESIGN, CONSTRUCTION, OPERATION	SCHROEDER, W.	01 0049	H
LIQUID FUEL, ECONOMICS, H-COAL		01 0507	H
LIQUID FUEL, ENVIRONMENT, COAL LIQUEFACTION	MAY, V.	01 0471	E
LIQUID FUEL, ENVIRONMENT, SNG	HEYCHUK, M.	01 0728	H
LIQUID FUEL, GASEOUS FUEL, FROM WASTE	HUNDEMANN, A.	01 0470	B
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LIQUID FUEL, HYDRODESULFN., HYDROCRACKING, HANDLING, SRC	GRESKOVICH, E.	01 0625	H
LIQUID FUEL, HYDROGENATION, WESTERN COAL, DILUTE PHASE		01 0206	H
LIQUID FUEL, LITLLE, A.D., COKING, EXTRACTIVE	KEBER, S.	01 0401	H
LIQUID FUEL, PRODN., ECONOMICS, BUR. OF MINES, SRC		01 0501	H
LIQUID FUEL, SNG PRODN., SRC HYDROLIQUEFACTION, PLANT	FASS, S.	01 0814	H
LIQUID FUEL, SNG, LNG, PROCESS	BEYCHOK, M.	01 0702	H
LIQUID FUEL, SOLID FUEL, PREPN. FROM COAL		01 0001	H
LNG, PROCESS, LIQUID FUELS, SNG	BEYCHOK, M.	01 0702	H
LURGI, BIOLOGICAL PURIFICATION, EFFLUENTS	GRAHAM, P.	01 0697	E
LURGI, COAL GASIFICATION, PHENOSOLVAN PROCESS	BEYCHOK, M.	01 0830	E
LURGI, DESIGN, COAL PLANT		01 0692	H
LURGI, EMISSIONS, HAZARDOUS, COKING, HEALTH, SRC	TAM, S.	01 0037	H
LURGI, EVALN., POLLUTION, CONTROL	MAGEE, E.	01 0035	H
LURGI, GASIFICATION REACTOR, DESIGN	YOON, H.	01 0341	E
LURGI, GASIFIER, AMERICAN COALS, WESTFIELD SCOTLAND		01 0143	H
LURGI, NEW SOURCE PERFORMANCE STANDARDS	SINOR, J.	01 0552	H
LURGI, SNG, WESTFIELD PLANT SUCCESS	GRAY, J.	01 0798	H
LURGI, SYNTHANE, BIGAS, CO(2) ACCEPTOR, DESIGN, COST	DETMAN, R.	01 0294	H
LURGI, SYNTHANE, BIGAS, CO(2) ACCEPTOR, FLOW DIAGRAMS	DETMAN, R.	01 0295	H
LURGI, SYNTHANE, HYGAS, CO(2) ACCEPTOR, KOPPERS	KIM, B.	01 0329	H
LURGI, 250 MILLION SCFD GAS PLANT, ECONOMICS		01 0390	H
MEMBRANE, ASPHALT, WASTE, DISPOSAL, LINERS	GESWEIN, A.	01 0519	H
MEMBRANE, COAL CONVERSION	SCHELL, W.	01 0626	H
MEMBRANE, ION EXCHANGE, DESALTING PROCESSES	CURRAN, H.	01 0790	H

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MEMBRANE, SLUDGE, POWER PLANT, WASTEWATER, REUSE	WELCH, P.	01 0517	E
MEMBRANE, WASTEWATER, DIALYSIS	DESAI, S.	01 0542	H
MEMBRANE, WATERWATER, PHENOL, REMOVAL		01 0759	E
METAL, ALLOYS, CORROSION, PHASE STABILITY DIAGRAMS	PERKINS, R.	01 0840	H
METAL, RECOVERY, INCINERATOR RESIDUE, WASTE, SOLID	GARBE, Y.	01 0533	H
METAL, SEPARATION, ION EXCHANGE	CALMON, C.	01 0907	E
METHANATION, COAL CHAR, COAL CLEANING, HYGAS, FUEL GAS		01 0211	H
METHANATION, HOT-GAS RECYCLE, EVALN., COAL GASIFICATION		01 0137	H
METHANATION, LIQUID PHASE		01 0002	H
METHANATION, LIQUID PHASE		01 0284	H
METHANATION, LIST OF REPORTS, COAL GASIFICATION	DETMAN, R.	01 0593	B
METHANATION, SINGLE-STAGE TUBE WALL, COAL GASIFICATION		01 0138	H
METHANATION, TUBE WALL, SYNTHANE	CHEN, J.	01 0136	E
METHANATION, WET, EVALN.	BRAUN, C.	01 0667	H
METHANE, ANAEROBIC FERMENTATION	HATFIELD, W.	01 0863	E
METHANE, EPA, WASTE, SOLID, SLUDGE, ANAEROBIC DIGESTION	HITTE, S.	01 0491	H
METHANOL, COAL GASIFICATION, PLANT DESIGN		01 0660	H
METHANOL, CONVERSION TO GASOLINE	VOLTZ, S.	01 0281	H
MEYERS, DESULFN., PROCESS DEVELOPMENT	KOUTSOUKOS, E.	01 0276	H
MEYERS, DESULFN., SURVEY OF 15 COALS	HAMERSMA, J.	01 0258	H
MEYERS, PHYSICAL ASPECTS, PROCESSES, COAL CLEANING		01 0275	H
MEYERS, POLLUTION CONTROL, EVALN.	MAGEE, E.	01 0297	H
MOLTEN SALT, FUEL CELL, DIRECT USE OF COAL	WEAVER, R.	01 0389	H
MOLTEN SALT, SCRUBBING	LESSING, L.	01 0044	E

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MOLTEN SALT, SCRUBBING, EMISSIONS, PROCESS		01 0117	H
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NATURAL GAS, FUEL, RESOURCES	GARRETT, R.	01 0633	E
NATURAL GAS, SOUR, SWEETENED BY CATACARB PROCESS PLANTS	EICKEMEYER, A.	01 0561	E
NATURAL GAS, SURVEY		01 0149	H
NITROGEN OXIDES, ABSORPTION-REDUCTION SCRUBBING	SEKIYA, T.	01 0904	E
NITROGEN OXIDES, EMISSIONS FROM FIXED FIREBOXES	SIDDIGI, A.	01 0578	E
NITROGEN OXIDES, POLLUTION CONTROL, AICHE SYMPOSIUM	SAROFIM, A.	01 0902	E
NITROGEN OXIDES, POLLUTION CONTROL, CONFERENCE		01 0901	E
NITROGEN, CONTROL, WASTEWATER TREATMENT, DESIGN MANUAL		01 0869	H
NITROGEN, OZONE EFFECT ON EFFLUENTS	WACHS, A.	01 0925	E
NITROGEN, REMOVAL, COAL LIQUIDS	SATCHELL, D.	01 0232	H
NITROGEN, REMOVAL, WASTEWATER		01 0497	H
NITROGEN, REMOVAL, WASTEWATER		01 0498	H
NITROGEN, ROLE IN ACTIVATED SLUDGE	WU, Y.	01 0921	E
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OIL SHALE, COAL CLEANING, SCRUBBING, WASTEWATER		01 0734	H
OIL SHALE, DISPOSAL, PARAHO, DEVELOPMENT ENGINEERING	HOLTZ, W.	01 0504	H
OIL SHALE, ENVIRONMENT, MEETING		01 0369	H
OIL SHALE, ERDA, COAL, ENERGY, REPORT		01 0310	H
OIL SHALE, FUEL GAS, HYDROGASIFICATION	FELDKIRCHNER, H.	01 0156	E
OIL SHALE, HYDROGEN, COAL GASIFICATION, ENVIRONMENT	DICKSON, E.	01 0321	H
OIL SHALE, PIPELINE GAS PRODN., HIGH PRESSURE	TSAROS, C.	01 0186	E

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OIL SHALE, RETORTING, IN SITU	HURWELL, E	01 0004	H
OIL SHALE, SRC, PRODUCTS & WASTES CHARACTERIZATION	FRUCHTER, J.	01 0628	H
OIL SHALE, TAR SANDS	SMITH, J.	01 0516	E
OIL SHALE, TAR SANDS, PROCESS EVALN.		01 0222	H
OIL SHALE, TAR SANDS, WESTERN STATES, COAL MINING	CORSENTINO, J.	01 0484	H
OIL SHALE, TAR, CHEMISTRY + TECHNOLOGY	ZELENIN, N.	01 0449	H
OIL SHALE, WASTEWATER, RECLAMATION, METHOD	HUBBARD, A.	01 0431	E
OIL, METAL CONTAINING WASTEWATER, TREATMENT	FORD, D.	01 0806	H
OIL, SEPARATION FROM WASTEWATER	LAWSON, J.	01 0807	E
OIL, WATER, SEPARATOR, GRAVITY, DESIGN	THOMSON, S.	01 0882	E
OXYGEN, ACTIVATED SLUDGE, FMC PROCESS	STETZER, R.	01 0915	E
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OZONE, CHLORINE, WATER DISINFECTION, CHEM/BIOLOGICAL EFF.	CARLSON, R.	01 0809	H
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OZONE, WASTEWATER TREATMENT, SECONDARY EFFLUENTS	HUIBERS, D.	01 0962	H
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PULLMAN KELLOGG INFORMATION STORAGE AND RETRIEVAL SYSTEM
RESEARCH INFORMATION DIVISION
FILE---01 EPA 68-02-2198 FUEL CONVERSION
INFORMATION ARRANGED BY SUBJECT

DATE---SEPTEMBER 1979

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PHENOL, REMOVAL, HYGAS, WASTEWATER, TREATMENT	LUTHY, R.	01 0755	H
PHENOL, REMOVAL, MEMBRANE, WASTEWATER		01 0759	E
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PHENOL, REMOVAL, WASTEWATER, STATE-OF-ART	SYLVESTER, N.	01 0642	H
PHENOL, WASTE TREATMENT	KLEMETSON, S.	01 0954	E
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PHENOL, WASTE, TREATMENT, TRICKLING FILTERS	JOYCE, T.	01 0478	E
PHENOL, WASTEWATER CONTAMINANTS, CONTROL	SINGER, P.	01 0794	H
PHENOL, WASTEWATER, PROCESSING, SYMPOSIUM		01 0669	E
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PNA, PROJECT SEACOKE, HYDROTREATING		01 0045	H
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POLLUTION, AIR, DATA PROCESSING SYSTEMS		01 0335	H
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POLLUTION, COAL, POWER PLANT, BASELINE DATA		01 0454	H
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POLLUTION, CONTROL, COAL GASIFICATION, COAL LIQUEFACTION	MAGEE, E.	01 0287	H
POLLUTION, CONTROL, EFFLUENTS, FUEL CONVERSION		01 0609	H
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POLLUTION, CONTROL, EVALN., SRC	JAHNIG, C.	01 0034	H
POLLUTION, CONTROL, EVALN., SYNTHANE	MAGEE, E.	01 0027	H
POLLUTION, CONTROL, EVALN., UGAS	JAHNIG, C.	01 0298	H
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POLLUTION, ENVIRONMENT, FUEL CONVERSION	HUNDEMANN, A.	01 0482	B
POLLUTION, FIXED BED SINGLE-STAGE COAL GASIFICATION	PAGE, G.	01 0941	E
POLLUTION, INDUSTRIAL, CONTROL, HANDBOOK	LUND, H.	01 0900	J
POLLUTION, ION TRANSPORT IN SOILS	NOVAK, L.	01 0736	E
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POLLUTION, MEASUREMENT, BOD, COD, TOC, TOD, COMPARISON	DAVIS, E.	01 0878	E
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POLLUTION, SCRUBBING, DESULFN., FLUE GAS		01 0618	H
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POLLUTION, TRACE ELEMENTS, NITROGEN, SULFUR	MAGEE, E.	01 0590	H
POLLUTION, WASTEWATER, GROUNDWATER MONITORING	TODD, D.	01 0690	H
POLLUTION, WASTEWATER, POWER PLANT, FLUE GAS, SCRUBBING	LEO, P.	01 0709	H
POLLUTION, WASTEWATER, SLUDGE, EFFLUENTS, TECHNOLOGY		01 0612	H
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POWER PLANT, BASELINE DATA, POLLUTION		01 0454	H
POWER PLANT, COAL GASIFICATION, COAL LIQUEFACTION		01 0145	H
POWER PLANT, COAL GASIFICATION, COAL LIQUEFACTION	BRIGGS, D	01 0289	H
POWER PLANT, COAL GASIFICATION, GAS CLEANING		01 0302	H

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POWER PLANT, COAL GASIFICATION, LOW-BTU	LEMEZIS, S.	01 0543	H
POWER PLANT, COAL GASIFICATION, WESTINGHOUSE		01 0502	H
POWER PLANT, COAL-FIRED, ASH CHARACTERIZATION	PARKER, F.	01 0792	H
POWER PLANT, COMBINED CYCLE, COAL GASIFICATION		01 0260	H
POWER PLANT, COMBINED CYCLE, ECONOMICS, ENVIRONMENT, SRC	REDDY, G.	01 0695	E
POWER PLANT, COOLING TOWER, BLOWDOWN	BOIES, D.	01 0014	H
POWER PLANT, COOLING TOWERS, ENVIRONMENT	HUNDEMANN, A.	01 0760	B
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POWER PLANT, ELECTROSTATIC PRECIPITATORS, DUST COLLECTION	TASSICKER, O.	01 0368	H
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POWER PLANT, FBC, LARGE STEAM GENERATORS	LAPPLE, W.	01 0772	H
POWER PLANT, FBC, LARGE STEAM GENERATORS	LAPPLE, W.	01 0773	H
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POWER PLANT, FLUE GAS, SCRUBBING, LEACHING, POLLUTION	ROSSOFF, J.	01 0709	H
POWER PLANT, FOSTER WHEELER, COAL GASIFICATION	SMITH, D.	01 0420	H
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POWER PLANT, GAS TURBINE, FUEL, COSTS	HEDLEY, W.	01 0016	H
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POWER PLANT, NUCLEAR, WASTE, SOLID, IMMOBILIZATION	NEILSON, R.	01 0664	E
POWER PLANT, OPEN CYCLE, COAL FIRED MHD		01 0236	H
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POWER PLANT, WASTEWATER, REUSE, MEMBRANE, SLUDGE	WELCH, P.	01 0517	E
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PYRITE, FLOTATION, CONC, PULP	MILLER, K.	01 0381	H
PYRITE, FLOTATION, TWO-STAGE PROCESS	MILLER, K.	01 0309	I
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PYRITE, REMOVAL, COAL CLEANING, PROCESS EVALN.		01 0327	H
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PYRITE, SEPARATION, WASHING, COAL CLEANING		01 0370	B
PYRITE, SULFUR, PROCESS ECONOMICS		01 0202	H
PYRITE, SULFUR, PROCESS ECONOMICS		01 0203	H
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REGULATIONS, COAL PLANTS		01 0730	H
REGULATIONS, COAL, AIR + WATER POLLUTION CONTROL, HEALTH		01 0416	H
REGULATIONS, EFFLUENTS	LOY, L.	01 0456	E
REGULATIONS, EFFLUENTS, POWER PLANT	NICHOLS, C.	01 0676	H
REGULATIONS, ENERGY SUPPLY & ENVIRONMENT COORDINATION ACT		01 0847	H
REGULATIONS, ENERGY SUPPLY & ENVIRONMENTAL COORDINATN. ACT		01 0846	H
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REGULATIONS, ENVIRONMENT, PRETREATMENT	BUSSE, R.	01 0643	H
REGULATIONS, ENVIRONMENT, WASTE, COAL, TECHNOLOGY SEMINAR		01 0668	H
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REGULATIONS, POLLUTION, AIR, NORTHERN GREAT PLAINS		01 0314	H
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SAFETY, HAZARDOUS MATERIALS, INDEX, TOXICITY	SAX, N.	01 0656	J
SAFETY, HEALTH, COAL CONVERSION	YOUNG, R.	01 0544	E
SAFETY, HYDROGENATION, COAL, HEALTH HAZARDS	SEXTON, R.	01 0447	E
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SCRUBBER, PARTICULATE, HOW TO CHOOSE	CALVERT, S.	01 0784	E
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SCRUBBING, DESULFN., FLUE GAS	KOEHLER, G.	01 0555	E
SCRUBBING, DESULFN., FLUE GAS, POLLUTION		01 0618	H
SCRUBBING, DESULFN., FLUE GAS, POLLUTION		01 0619	H
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SCRUBBING, EMISSIONS, PROCESS, MOLTEN SALT		01 0117	H
SCRUBBING, FOAM, FINE PARTICULATE CONTROL	CTVRTNICEK, T.	01 0781	E
SCRUBBING, GAS CLEANING, MERC GASIFIER	MOORE, A.	01 0616	H
SCRUBBING, HYDROGEN SULFIDE REGENERATION, SULFUR PRODN. ROC	HELLE, G.	01 0861	E
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SCRUBBING, LIMESTONE, LIME, OXIDN., EPA.	HEAD, H	01 0753	E
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01 0718	AEROSPACE CORP.
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01 0722	AICHE NATL. MEETING 82
01 0635	AICHE, GWDA, EPA, INFORMATION TRANSFER, UNIV. OF HOUSTON
01 0368	AIR POLLUTION SYSTEMS, INC
01 0784	AIR POLLUTION TECHNOLOGY, INC.
01 0011	AIR PRODUCTS AND CHEMICALS, INC.
01 0141	AIR PRODUCTS AND CHEMICALS, INC.
01 0241	AIR PRODUCTS AND CHEMICALS, INC.
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01 0403	AIR PRODUCTS AND CHEMICALS, INC.
01 0625	AIR PRODUCTS AND CHEMICALS, INC.
01 0638	AIR PRODUCTS AND CHEMICALS, INC.
01 0962	AIR REDUCTION CO.
01 0741	AIRCO INDUSTRIAL GASES
01 0691	ALLIED CHEMICAL-INDUSTRIAL CHEMICALS DIVISION
01 0800	AMERICAN IRON AND STEEL INSTITUTE
01 0069	AMOCO
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01 0834	ARGONNE NATL LABORATORY
01 0904	ASAHI CHEMICAL INDUSTRY CO., LTD.
01 0465	ASHLAND OIL
01 0226	ASSOCIATED UNIVERSITIES, INC.
01 0045	ATLANTIC RICHFIELD CO.
01 0046	ATLANTIC RICHFIELD CO.
01 0047	ATLANTIC RICHFIELD CO.
01 0578	ATLANTIC RICHFIELD CO.
01 0116	ATOMICS INTL.
01 0117	ATOMICS INTL.
01 0030	AUBURN UNIV.
01 0789	AUTOTROL CORP.
01 0235	AVCO EVERETT RESEARCH LAB.
01 0112	AVCO SPACE SYSTEMS DIVISION
01 0668	AWARE
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01 0918	AWARE
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01 0967	AWARE
01 0413	BABCOCK & WILCOX
01 0700	BABCOCK & WILCOX
01 0701	BABCOCK & WILCOX
01 0772	BABCOCK & WILCOX
01 0773	BABCOCK & WILCOX
01 0660	BADGER CO., INC.
01 0490	BARTLESVILLE ENERGY RESEARCH CENTER
01 0018	BATTELLE
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01 0628	BATTELLE PACIFIC NORTHWEST LAB.
01 0385	BATTELLE-COLUMBUS LABORATORIES
01 0203	BECHTEL CORP.
01 0380	BECHTEL CORP.
01 0753	BECHTEL CORP.
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01 0366	BOLT BERANEK AND NEWMAN, INC.
01 0094	BOOZ-ALLEN & HAMILTON, INC.
01 0095	BOOZ-ALLEN & HAMILTON, INC.
01 0315	BOOZ-ALLEN & HAMILTON, INC.
01 0606	BOOZ-ALLEN & HAMILTON, INC.
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01 0294	BRAUN, C.F. & CO.
01 0295	BRAUN, C.F. & CO.
01 0296	BRAUN, C.F. & CO.
01 0593	BRAUN, C.F. & CO.
01 0620	BRAUN, C.F. & CO.
01 0667	BRAUN, C.F. & CO.
01 0687	BRAUN, C.F. & CO.
01 0823	BRAUN, C.F. & CO.
01 0799	BRIGHAM YOUNG UNIV.
01 0243	BRIGHAM-YOUNG UNIV.
01 0798	BRITISH GAS CORP.
01 0151	BRITISH STEEL CORP.
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01 0135	BUR. OF MINES
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01 0364	BUR. OF MINES
01 0375	BUR. OF MINES
01 0381	BUR. OF MINES
01 0406	BUR. OF MINES
01 0418	BUR. OF MINES
01 0431	BUR. OF MINES
01 0484	BUR. OF MINES
01 0501	BUR. OF MINES
01 0507	BUR. OF MINES
01 0538	BUR. OF MINES
01 0596	BUR. OF MINES
01 0632	BUR. OF MINES
01 0159	BUR. OF MINES MANAGING COAL WASTES & POLLUTION PROGRAM
01 0345	BUR. OF RECLAMATION
01 0579	CALGON CORP.
01 0877	CALGON CORP.
01 0552	CAMERON ENGINEERS, INC.

ACCESSION NO.	CORPORATE AUTHOR
01 0696	CARNEGIE MELLON UNIV.- ENVIRONMENTAL STUDIES INSTITUTE
01 0820	CARNEGIE-MELLON
01 0342	CARNEGIE-MELLON UNIV.
01 0699	CARNEGIE-MELLON UNIV.
01 0879	CARNEGIE-MELLON UNIV.
01 0885	CARNEGIE-MELLON UNIV.
01 0944	CARNEGIE-MELLON UNIV.
01 0948	CARNEGIE-MELLON UNIV.
01 0684	CASE WESTERN RESERVE UNIV.
01 0607	CATALYTIC, INC.
01 0609	CATALYTIC, INC.
01 0704	CATALYTIC, INC.
01 0950	CATALYTIC, INC.
01 0002	CHEM SYSTEMS INC.
01 0076	CHEM SYSTEMS INC.
01 0284	CHEM SYSTEMS INC.
01 0742	CHEVRON RESEARCH CO.
01 0965	CHEVRON RESEARCH CO.
01 0581	CHIYODA
01 0924	CLEMSON UNIV.
01 0833	CLEVELAND REGIONAL SEWER DISTRICT
01 0736	CLEVELAND STATE UNIV.
01 0441	COAL RESEARCH BUREAU
01 0854	COALCON
01 0267	COLORADO INTERSTATE GAS CO.

ACCESSION NO.	CORPORATE AUTHOR
01 0324	COLORADO STATE UNIV.
01 0954	COLORADO STATE UNIV.
01 0750	COLUMBUS & SOUTHERN OHIO ELECTRIC
01 0261	COMBUSTION ENGINEERING
01 0487	COMBUSTION ENGINEERING
01 0451	COMBUSTION ENGINEERING, INC.
01 0205	COMBUSTION POWER CO.
01 0308	COMMITTEE ON MEDICAL AND BIOLOGIC EFFECTS OF ENVIRONMENTAL POLLUTANTS
01 0778	CONOCO
01 0448	CONOCO COAL DEVELOPMENT CO.
01 0032	CONSOLIDATION COAL CO.
01 0051	CONSOLIDATION COAL CO.
01 0052	CONSOLIDATION COAL CO.
01 0053	CONSOLIDATION COAL CO.
01 0118	CONSOLIDATION COAL CO.
01 0120	CONSOLIDATION COAL CO.
01 0125	CONSOLIDATION COAL CO.
01 0126	CONSOLIDATION COAL CO.
01 0127	CONSOLIDATION COAL CO.
01 0128	CONSOLIDATION COAL CO.
01 0129	CONSOLIDATION COAL CO.
01 0167	CONSOLIDATION COAL CO.
01 0168	CONSOLIDATION COAL CO.
01 0169	CONSOLIDATION COAL CO.
01 0170	CONSOLIDATION COAL CO.

ACCESSION NO.	CORPORATE AUTHOR
01 0677	CONSOLIDATION COAL CO.
01 0540	CORNELL UNIV.
01 0386	CORVALLIS ERL
01 0831	DAMES & MOORE
01 0300	DAVIS, J.J., ASSOCIATES
01 0504	DEVELOPMENT ENGINEERING INC. & WOODWARD-CLYDE CONSULTANTS
01 0599	DOW CHEMICAL CO.
01 0764	DOW CHEMICAL CO.
01 0770	DOW CHEMICAL CO.
01 0266	DRAVO CORP.
01 0288	DRAVO CORP.
01 0412	DRAVO CORP.
01 0442	DRAVO CORP.
01 0682	DUPONT
01 0860	DUPONT
01 0166	DYNATECH
01 0365	EASTERN ASSOCIATED COAL CORP.
01 0637	EBON RESEARCH SYSTEMS
01 0893	ECODYNE COOLING PRODUCTS CO.
01 0917	ECODYNE CORP.
01 0630	ECONERGY ASSOCIATES
01 0916	EDC/ENVIRO DEVELOPMENT CO., INC.
01 0884	EL PASO ENVIRONMENTAL SYSTEMS, INC.
01 0730	EMISSION STANDARDS & ENGINEERING DIVISION
01 0731	EMISSION STANDARDS AND ENGINEERING DIVISION

ACCESSION NO.	CORPORATE AUTHOR
01 0655	EMSL
01 0455	ENERGY RESOURCES CO. INC.
01 0801	ENGINEERING SCIENCE, INC.
01 0744	ENGINEERING-SCIENCE CO.
01 0782	ENTOLETER, INC.
01 0785	ENTOLETER, INC.
01 0546	ENVIREX INC.
01 0626	ENVIROGENICS SYSTEMS
01 0446	ENVIRONMENTAL MONITORING AND SUPPORT LABORATORY
01 0478	ENVIROTECH CORP.
01 0886	ENVIROTECH CORP.
01 0865	ENVIROTECH PROCESS EQUIPMENT
01 0636	ENVIROTECH, EIMCO BSP DIVISION
01 0350	EPA
01 0376	EPA
01 0475	EPA
01 0486	EPA
01 0488	EPA
01 0491	EPA
01 0495	EPA
01 0497	EPA
01 0498	EPA
01 0500	EPA
01 0508	EPA
01 0509	EPA

ACCESSION NO.	CORPORATE AUTHOR
01 0519	EPA
01 0528	EPA
01 0529	EPA
01 0533	EPA
01 0547	EPA
01 0548	EPA
01 0603	EPA
01 0643	EPA
01 0765	EPA
01 0934	EPA
01 0550	EPA-LIBRARY SYSTEMS BRANCH
01 0835	EPA, OFF. WATER PROGRAM OPERATIONS
01 0712	EPA, RUTGERS UNIV.
01 0153	ERDA
01 0216	ERDA
01 0217	ERDA
01 0218	ERDA
01 0224	ERDA
01 0247	ERDA
01 0310	ERDA
01 0311	ERDA
01 0428	ERDA
01 0438	ERDA
01 0483	ERDA
01 0511	ERDA

ACCESSION NO.	CORPORATE AUTHOR
01 0539	ERDA
01 0027	ESSO RESEARCH & ENGINEERING CO.
01 0304	ESSO RESEARCH & ENGINEERING CO.
01 0590	ESSO RESEARCH & ENGINEERING CO.
01 0033	EXXON
01 0034	EXXON
01 0035	EXXON
01 0200	EXXON
01 0207	EXXON
01 0219	EXXON
01 0220	EXXON
01 0287	EXXON
01 0297	EXXON
01 0298	EXXON
01 0301	EXXON
01 0362	EXXON
01 0387	EXXON
01 0580	EXXON
01 0825	EXXON
01 0903	EXXON
01 0844	EXXON RESEARCH AND ENGINEERING CO.
01 0338	EYRING RESEARCH INST.
01 0377	FEDERAL ENERGY ADMINISTRATION
01 0846	FEDERAL ENERGY ADMINISTRATION
01 0847	FEDERAL ENERGY ADMINISTRATION

ACCESSION NO.	CORPORATE AUTHOR
01 0586	FEDERAL POWER COMMISSION
01 0618	FEDERAL POWER COMMISSION
01 0619	FEDERAL POWER COMMISSION
01 0142	FLUOR
01 0228	FLUOR
01 0234	FLUOR
01 0240	FLUOR
01 0272	FLUOR
01 0629	FLUOR
01 0802	FLUOR
01 0832	FLUOR
01 0857	FLUOR
01 0898	FLUOR
01 0882	FLUOR ENGINEERS & CONSTRUCTORS, INC.
01 0421	FLUOR UTAH
01 0054	FMC CORP.
01 0055	FMC CORP.
01 0056	FMC CORP.
01 0057	FMC CORP.
01 0059	FMC CORP.
01 0278	FMC CORP.
01 0515	FMC CORP.
01 0915	FMC CORP.
01 0424	FORD, BACON, & DAVIS, INC.
01 0082	FOSTER WHEELER CORP.

ACCESSION NO.	CORPORATE AUTHOR
01 0204	FOSTER WHEELER CORP.
01 0260	FOSTER WHEELER CORP.
01 0420	FOSTER WHEELER CORP.
01 0841	FOSTER WHEELER CORP.
01 0859	FOSTER WHEELER ENERGY CORP.
01 0165	FRANKLIN INST.
01 0639	GARD INC.
01 0651	GENERAL ANALYTICS
01 0253	GENERAL ELECTRIC
01 0672	GENERAL ELECTRIC
01 0690	GENERAL ELECTRIC
01 0527	GENERAL TIRE AND RUBBER
01 0469	GILBERT ASSOCIATES
01 0512	GOAR, ARRINGTON & ASSOCIATES, INC.
01 0604	GOODYEAR ATOMIC CORP.
01 0008	GRAND FORKS ERL
01 0028	GRAND FORKS ERL
01 0551	GULF OIL CORP.
01 0818	GULF RESEARCH AND DEVOLOPMENT CO.
01 0542	GULF SOUTH RESEARCH INST.
01 0914	GULF STATES PAPER CORP.
01 0530	HERCULES, INC.
01 0041	HITTMAN ASSOC., INC.
01 0042	HITTMAN ASSOC., INC.
01 0430	HITTMAN ASSOC., INC.

ACCESSION NO.	CORPORATE AUTHOR
01 0454	HITTMAN ASSOC., INC.
01 0471	HITTMAN ASSOC., INC.
01 0698	HITTMAN ASSOC., INC.
01 0790	HITTMAN ASSOC., INC.
01 0853	HITTMAN ASSOC., INC.
01 0939	HITTMAN ASSOC., INC.
01 0942	HITTMAN ASSOC., INC.
01 0545	HORMEL, G.A. & CO.
01 0060	HYDROCARBON RESEARCH
01 0061	HYDROCARBON RESEARCH
01 0066	HYDROCARBON RESEARCH
01 0070	HYDROCARBON RESEARCH
01 0171	HYDROCARBON RESEARCH
01 0229	HYDROCARBON RESEARCH
01 0277	HYDROCARBON RESEARCH
01 0602	HYDROCARBON RESEARCH
01 0662	HYDROCARBON RESEARCH
01 0811	HYDROCARBON RESEARCH
01 0899	HYDROCARBON RESEARCH
01 0928	ICI AMERICA INC.
01 0230	IERL
01 0716	IERL
01 0725	IERL
01 0727	IERL
01 0738	IERL

ACCESSION NO.	CORPORATE AUTHOR
01 0754	IERL
01 0693	IERL-ENERGY ASSESSMENT & CONTROL DIVISION
01 0150	IGT
01 0156	IGT
01 0160	IGT
01 0161	IGT
01 0162	IGT
01 0163	IGT
01 0164	IGT
01 0186	IGT
01 0190	IGT
01 0191	IGT
01 0192	IGT
01 0193	IGT
01 0194	IGT
01 0195	IGT
01 0196	IGT
01 0197	IGT
01 0199	IGT
01 0209	IGT
01 0210	IGT
01 0211	IGT
01 0212	IGT
01 0223	IGT
01 0286	IGT

ACCESSION NO.	CORPORATE AUTHOR
01 0322	IGT
01 0339	IGT
01 0395	IGT
01 0472	IGT
01 0479	IGT
01 0587	IGT
01 0591	IGT
01 0673	IGT
01 0012	ILLINOIS STATE GEOLOGICAL SURVEY
01 0439	ILLINOIS STATE GEOLOGICAL SURVEY
01 0665	ILLINOIS STATE GEOLOGICAL SURVEY
01 0739	ILLINOIS STATE GEOLOGICAL SURVEY
01 0953	ILLINOIS STATE GEOLOGICAL SURVEY
01 0957	ILLINOIS STATE GEOLOGICAL SURVEY
01 0407	ILLINOIS UNIVERSITY
01 0863	ILLINOIS, DIV. OF STATE WATER SURVEY
01 0363	IMMR
01 0425	IMMR
01 0335	INDEX SYSTEMS INC.
01 0427	INPUT OUTPUT COMPUTER SERVICES, INC.
01 0819	INSTITUTE FOR ENERGY ANALYSIS
01 0158	IOWA STATE UNIV.
01 0496	IOWA STATE UNIV.
01 0925	ISRAEL INST. OF TECHNOLOGY
01 0694	IU CONVERSION SYSTEMS, INC.

ACCESSION NO.	CORPORATE AUTHOR
01 0850	IU CONVERSION SYSTEMS, INC.
01 0459	JOCOBS ENGINEERING CO.
01 0242	JOHNS-MANVILLE SALES CORPERATION
01 0467	KAISER ENGINEERS
01 0839	KAISER STEEL CORP.
01 0145	KELLOGG
01 0155	KELLOGG
01 0173	KELLOGG
01 0174	KELLOGG
01 0732	KELLOGG
01 0895	KELLOGG
01 0952	KELLOGG
01 0344	KENTUCKY UNIV.
01 0408	KVH ENGINEERING, INC.
01 0402	LAWRENCE LIVERMORE LABORATORY
01 0452	LAWRENCE LIVERMORE LABORATORY
01 0489	LEHIGH UNIV.
01 0004	LERC
01 0202	LITTLE, A.D.
01 0401	LITTLE, A.D.
01 0666	LITTLE, A.D.
01 0724	LITTLE, A.D.
01 0851	LITTLE, A.D., INC.
01 0422	LOCKHEED MISSILES & SPACE CO. INC.
01 0713	LOCKHEED MISSILES & SPACE CO. INC.

ACCESSION NO.	CORPORATE AUTHOR
01 0840	LOCKHEED PALO ALTO RESEARCH LAB.
01 0763	LOUISIANA CHEMICAL ASSOC.
01 0136	LUMMUS CO.
01 0265	LUMMUS CO.
01 0689	LUMMUS CO.
01 0373	MARCOM
01 0426	MARYLAND DEPT. OF HEALTH AND MENTAL HYGIENE
01 0494	MATRECON, INC.
01 0340	MCGILL UNIV.
01 0783	MCILVAINE CO.
01 0958	MCKEE, ARTHUR G. & CO.
01 0966	MCKEE, ARTHUR G. & CO.
01 0318	MCNALLY PITTSBURG MFG. CORP.
01 0319	MCNALLY PITTSBURG MFG. CORP.
01 0175	MELPAR, INC.
01 0097	MERC
01 0333	MERC
01 0415	MERC
01 0616	MERC
01 0317	MERL
01 0708	MERL
01 0595	METALLGESELLSCHAFT AG
01 0305	MINNESOTA UNIV.
01 0236	MIT
01 0245	MIT

ACCESSION NO.	CORPORATE AUTHOR
01 0312	MITRE CORP.
01 0640	MITRE CORP.
01 0733	MITRE CORP.
01 0913	MOBAY CHEMICAL CORP.
01 0281	MOBIL
01 0251	MOBIL R&D CORP.
01 0016	MONSANTO RESEARCH CORP.
01 0017	MONSANTO RESEARCH CORP.
01 0040	MONSANTO RESEARCH CORP.
01 0781	MONSANTO RESEARCH CORP.
01 0752	MONTANA POWER CO.
01 0131	MORGANTOWN COAL RESEARCH CENTER
01 0132	MORGANTOWN COAL RESEARCH CENTER
01 0137	MORGANTOWN RESEARCH CENTER
01 0138	MORGANTOWN RESEARCH CENTER
01 0894	MORRISON-KNUDSEN CO., INC.
01 0759	N. DAKOTA STATE UNIV.
01 0862	N.J. INSTITUTE OF TECHNOLOGY
01 0697	NAT'L. COAL BOARD, UNITED KINGDOM
01 0177	NATHAN ASSOCIATES, INC
01 0714	NATIONAL SCIENCE FOUNDATION
01 0358	NATL BUR. OF STANDARDS
01 0396	NAVEL AIR PROPULTION TEST CENTER
01 0089	NERC
01 0702	NERC

ACCESSION NO.	CORPORATE AUTHOR
01 0719	NERC
01 0867	NERC
01 0293	NEW MEXICO STATE UNIV.
01 0544	NIOSH
01 0617	NIOSH
01 0949	NORTH CAROLINA STATE UNIV.
01 0314	NORTHERN GREAT PLAINS RESOURCE PROGRAM
01 0238	NTIS
01 0249	NTIS
01 0256	NTIS
01 0470	NTIS
01 0911	NUS CORP.
01 0588	OEMI
01 0723	OFFICE OF ENVIRONMENTAL PROJECT REVIEW
01 0615	OFFICE OF SOLID WASTE
01 0231	OKLAHOMA STATE UNIV.
01 0232	OKLAHOMA STATE UNIV.
01 0233	OKLAHOMA STATE UNIV.
01 0663	OKLAHOMA STATE UNIV.
01 0292	ORNL
01 0306	ORNL
01 0393	ORNL
01 0437	ORNL
01 0453	ORNL
01 0461	ORNL

ACCESSION NO.	CORPORATE AUTHOR
01 0474	ORNL
01 0505	ORNL
01 0553	ORNL
01 0592	ORNL
01 0597	ORNL
01 0610	ORNL
01 0757	ORNL
01 0793	ORNL
01 0815	ORNL
01 0855	ORNL
01 0856	ORNL
01 0670	OWHM
01 0676	OWHM
01 0535	PACIFIC ENVIRONMENTAL SERVICES, INC.
01 0014	PACIFIC NORTWEST ERL
01 0468	PARKSON CORP. & CHILDRESS CORP.
01 0814	PARSONS, RALPH M. CO.
01 0837	PARSONS, RALPH M. CO.
01 0905	PARSONS, RALPH M. CO.
01 0951	PARSONS, RALPH M. CO.
01 0001	PARSONS, RALPH M., CO.
01 0072	PARSONS, RALPH M., CO.
01 0083	PARSONS, RALPH M., CO.
01 0323	PARSONS, RALPH M., CO.
01 0720	PARSONS, RALPH M., CO.

ACCESSION NO.	CORPORATE AUTHOR
01 0869	PEABODY ENGINEERED SYSTEMS
01 0959	PEABODY HOLMES CO.
01 0423	PEAT, MARWICK, MITCHELL, AND CO.
01 0842	PEDCO ENVIRONMENTAL SPECIALISTS, INC.
01 0499	PEDCO-ENVIRONMENTAL, INC.
01 0910	PENN ENVIRONMENTAL CONSULTANTS, INC.
01 0748	PENN. POWER CO.
01 0023	PENN. STATE UNIV.
01 0031	PENN. STATE UNIV.
01 0119	PENN. STATE UNIV.
01 0457	PENN. STATE UNIV.
01 0458	PENN. STATE UNIV.
01 0003	PERC
01 0005	PERC
01 0007	PERC
01 0010	PERC
01 0081	PERC
01 0085	PERC
01 0208	PERC
01 0326	PERC
01 0349	PERC
01 0352	PERC
01 0356	PERC
01 0361	PERC
01 0367	PERC

ACCESSION NO.	CORPORATE AUTHOR
01 0374	PERC
01 0382	PERC
01 0384	PERC
01 0397	PERC
01 0400	PERC
01 0503	PERC
01 0510	PERC
01 0514	PERC
01 0608	PERC
01 0797	PERC
01 0845	PERC
01 0817	PERMUTIT
01 0920	PHILADELPHIA ELECTRIC CO.
01 0657	PHILLIPS PETROLEUM CO.
01 0450	PHILLIPS PETROLIUM CO.
01 0922	PICKARD AND ANDERSON
01 0043	PITTSBURG & MIDWAY COAL MINING CO.
01 0071	PITTSBURG & MIDWAY COAL MINING CO.
01 0078	PITTSBURG & MIDWAY COAL MINING CO.
01 0079	PITTSBURG & MIDWAY COAL MINING CO.
01 0521	PITTSBURG & MIDWAY COAL MINING CO.
01 0522	PITTSBURG & MIDWAY COAL MINING CO.
01 0523	PITTSBURG & MIDWAY COAL MINING CO.
01 0524	PITTSBURG & MIDWAY COAL MINING CO.
01 0598	PITTSBURG & MIDWAY COAL MINING CO.

ACCESSION NO.	CORPORATE AUTHOR
01 0795	PITTSBURG & MIDWAY COAL MINING CO.
01 0796	PITTSBURG & MIDWAY COAL MINING CO.
01 0808	PITTSBURG & MIDWAY COAL MINING CO.
01 0926	PITTSBURG & MIDWAY COAL MINING CO.
01 0348	PITTSBURGH MINING & SAFETY RESEARCH CENTER
01 0881	POLYBAC CORP.
01 0392	PRINCETON UNIV.
01 0929	PURDUE UNIV.
01 0930	PURDUE UNIV.
01 0931	PURDUE UNIV.
01 0848	PURVIN AND GERTZ, INC.
01 0372	RADIAN CORP.
01 0394	RADIAN CORP.
01 0410	RADIAN CORP.
01 0534	RADIAN CORP.
01 0671	RADIAN CORP.
01 0703	RADIAN CORP.
01 0787	RADIAN CORP.
01 0788	RADIAN CORP.
01 0896	RADIAN CORP.
01 0897	RADIAN CORP.
01 0936	RADIAN CORP.
01 0937	RADIAN CORP.
01 0941	RADIAN CORP.
01 0683	RESEARCH TRIANGLE INST.

ACCESSION NO.	CORPORATE AUTHOR
01 0715	RESEARCH TRIANGLE INST.
01 0735	RESEARCH TRIANGLE INST.
01 0767	RESEARCH TRIANGLE INST.
01 0768	RESEARCH TRIANGLE INST.
01 0036	RESEARCH TRIANGLE INSTITUTE
01 0935	RESEARCH TRIANGLE INSTITUTE
01 0943	RESEARCH TRIANGLE INSTITUTE
01 0945	RESEARCH TRIANGLE INSTITUTE
01 0827	ROBERT S. KERR ERL
01 0807	ROY F. WESTON, INC.
01 0473	SANDIA LABS.
01 0048	SCHROEDER & ASSOCIATES
01 0049	SCHROEDER & ASSOCIATES
01 0227	SCIENTIFIC RESEARCH INSTRUMENTS CORP.
01 0178	SKEIST LABORATORIES, INC.
01 0456	SKELLY & LOY
01 0391	SOUTHEAST ENVIRONMENTAL RESEARCH LABORATORY
01 0769	SOUTHERN RESEARCH INSTITUTE
01 0766	SPOKANE MINING RESEARCH CENTER
01 0346	SPOKANE MINING RESEARCH INST.
01 0148	SSIE, INC.
01 0933	STANDARD OIL
01 0347	STANFORD RESEARCH INST
01 0369	STANFORD RESEARCH INST
01 0179	STANFORD RESEARCH INST.

ACCESSION NO.	CORPORATE AUTHOR
01 0388	STANFORD RESEARCH INST.
01 0389	STANFORD RESEARCH INST.
01 0492	STANFORD RESEARCH INST.
01 0804	STANFORD RESEARCH INST.
01 0890	STANFORD RESEARCH INST.
01 0122	STEARNS-ROGER CORP.
01 0123	STEARNS-ROGER CORP.
01 0577	STONE & WEBSTER ENG.
01 0302	STONE & WEBSTER ENGINEERING CORP.
01 0908	SUN OIL CO.
01 0360	SVERDRUP & PARCEL & ASSOCIATES
01 0399	TEKNEKRON, INC.
01 0526	TEXACO
01 0822	TOMSK MEDICAL INSTITUTE
01 0258	TRW
01 0276	TRW
01 0460	TRW
01 0404	TRW ENERGY SYSTEMS
01 0936	TRW INC.
01 0852	TRW, INC.
01 0485	TVA
01 0721	TVA
01 0751	TVA
01 0792	TVA
01 0960	TVA

ACCESSION NO.	CORPORATE AUTHOR
01 0729	TWIN CITIES METALLURGY RESEARCH CENTER
01 0379	TWIN CITIES MINING RESEARCH CENTER
01 0466	U.S. STEEL RESEARCH
01 0022	UCR, FOR. DEPT. OF INTERIOR
01 0299	UNION CARBIDE
01 0813	UNION CARBIDE
01 0816	UNION CARBIDE
01 0912	UNION CARBIDE CORP.
01 0919	UNION CARBIDE CORP.
01 0947	UNITED TECHNOLOGIES
01 0821	UNITED TECHNOLOGIES CHEMICAL SYSTEMS DIVISION
01 0398	UNITED TECHNOLOGIES RESEARCH CENTER
01 0291	UNIV. OF CALIF.
01 0330	UNIV. OF CALIF.
01 0331	UNIV. OF CALIF.
01 0332	UNIV. OF CALIF.
01 0435	UNIV. OF CALIF.
01 0594	UNIV. OF CALIF.
01 0624	UNIV. OF CALIF.
01 0861	UNIV. OF CALIF.
01 0029	UNIV. OF CALIFORNIA
01 0341	UNIV. OF DELAWARE
01 0417	UNIV. OF KENTUCKY
01 0537	UNIV. OF KENTUCKY
01 0273	UNIV. OF LOUISVILLE, KY.

ACCESSION NO.	CORPORATE AUTHOR
01 0289	UNIV. OF MICHIGAN
01 0809	UNIV. OF MINNESOTA
01 0433	UNIV. OF MONTANA
01 0434	UNIV. OF MONTANA
01 0444	UNIV. OF MONTANA
01 0745	UNIV. OF MONTANA
01 0613	UNIV. OF N. CAROLINA
01 0622	UNIV. OF N. CAROLINA
01 0794	UNIV. OF N. CAROLINA
01 0923	UNIV. OF N. CAROLINA
01 0955	UNIV. OF N. CAROLINA
01 0039	UNIV. OF N. DAKOTA
01 0946	UNIV. OF N. DAKOTA
01 0354	UNIV. OF N. MEXICO
01 0601	UNIV. OF NOTRE DAME
01 0864	UNIV. OF PITTSBURGH
01 0880	UNIV. OF PITTSBURGH
01 0921	UNIV. OF PITTSBURGH
01 0711	UNIV. OF TEXAS
01 0878	UNIV. OF TEXAS
01 0932	UNIV. OF TEXAS
01 0887	UNIV. OF TORONTO
01 0641	UNIV. OF TULSA
01 0642	UNIV. OF TULSA
01 0645	UNIV. OF TULSA

ACCESSION NO.	CORPORATE AUTHOR
01 0646	UNIV. OF TULSA
01 0647	UNIV. OF TULSA
01 0648	UNIV. OF TULSA
01 0649	UNIV. OF TULSA
01 0650	UNIV. OF TULSA
01 0805	UNIV. OF TULSA
01 0806	UNIV. OF TULSA
01 0086	UNIV. OF UTAH
01 0088	UNIV. OF UTAH
01 0206	UNIV. OF UTAH
01 0688	US AIR FORCE
01 0707	USDA, FOREST SERVICE
01 0557	USS ENGINEERS & CONSULTANTS, INC.
01 0776	VANDERBILT UNIV.
01 0463	VIRGINIA POLYTECHNIC INST. & STATE UNIV.
01 0771	WASHINGTON STATE UNIV.
01 0480	WATER PURIFICATION ASSOCIATES
01 0612	WATER PURIFICATION ASSOCIATES
01 0907	WATER PURIFICATION ASSOCIATES
01 0956	WATER PURIFICATION ASSOCIATES
01 0447	WEST VIRGINIA INST.
01 0183	WEST VIRGINIA UNIV.
01 0184	WEST VIRGINIA UNIV.
01 0443	WEST VIRGINIA UNIV.
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16. ABSTRACT

This volume is the product of an information-gathering effort relating to coal conversion process streams. Available and developing control technology has been evaluated in view of the requirements of present and proposed federal, state, regional, and international environmental standards. The study indicates that it appears possible to evolve technology to reduce each component of each process stream to an environmentally acceptable level. It also indicates that such an approach would be costly and difficult to execute. Because all coal conversion processes are net users of water, liquid effluents need be treated only for recycling within the process, thus achieving essentially zero discharge. With available technology, gaseous emissions can be controlled to meet present environmental standards, particulates can be controlled or eliminated, and disposal of solid wastes can be managed to avoid deleterious environmental effects. This volume (III) includes both a program for economic analysis of control technology and the appendix.

17. KEY WORDS AND DOCUMENT ANALYSIS

a. DESCRIPTORS	b. IDENTIFIERS/OPEN ENDED TERMS	c. COSATI Field/Group
Pollution	Pollution Control	13B
Coal Gasification	Stationary Sources	13H
Coal Preparation	Coal Conversion	13I
Economic Analysis		05C

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