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APPENDIX E AND F TO NETWORK DESIGN AND SITE EXPOSURE CRITERIA FOR SELECTED NONCRITERIA AIR POLLUTANTS



INTRODUCTION

This report contains Appendices E and F to the previously published "Network Design and Site Exposure Criteria for Selected Noncriteria Air Pollutants," EPA-450/4-84-022 (September 1984). Appendix E contains the chemical profiles for 20 new chemicals and Appendix F contains guidance on the monitoring frequency for noncriteria air pollutants.

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APPENDIX E

NETWORK DESIGN AND SITE EXPOSURE CRITERIA FOR SELECTED NONCRITERIA AIR POLLUTANTS

Prepared by

PEI Associates, Inc. 11499 Chester Road Cincinnati, Ohio 45246

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APPENDIX E

This appendix to the EPA report "Network Design and Site Exposure Criteria for Selected Noncriteria Air Pollutants" (EPA-450/4-84-022) dated September 1984 completes the chemical profiles begun in Appendix D; four completely new chemicals have been added. Sixteen chemicals were included in the body of the report for which no chemical profiles were included in Appendix D. Chemical profiles are included in this appendix for these chemicals and four additional pollutants: benzo(a)pyrene, 1,3-butadiene, ethylene dibromide, and 4,4'-methylenedianiline. The 20 chemicals included in this appendix are:

- ° benzo(a)pyrene
- ° 1,3-butadiene
- ° o-, m-, p-cresol
- ° p-dichlorobenzene
- ° dimethylnitrosamine
- ° ethylene dichloride
- ° ethylene dibromide
- ° ethylene oxide
- ° formaldehyde
- [°] hexachlorocyclopentadiene
- ° maleic anhydride
- ° manganese
- ° mercury
- ° methylene chloride
- ° 4,4'-methylenedianiline
- ° perchloroethylene
- ° phenol
- ° phosgene
- propylene oxide
- ° o-, m-, p-xylene

The information in this appendix has been reviewed by industry groups and reflects their comments.

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Chemical Name

Benzo(a)pyrene

CAS Number

50-32-8

Chemical Classification

Polynuclear aromatic hydrocarbon

Synonyms

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Benzo(d,e,f)chrysene, 3,4-benzopirene, 3,4-benzopyrene,
6,7-benzopyrene, 3,4 benzpyren, benz(a)pyrene, 3,4-benzpyrene,
3,4-benz(a)pyrene, 3,4-benzypyrene, BP, B(a)P, 3,4-BP
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Physical/Chemical Properties

Description: Yellowish crystals Boiling Point: 310° to 312°C (10mm) Melting Point: 179°C Molecular Weight: 252.3 Chemical Formula: $C_{12}H_{20}$ Vapor Pressure: 5.49×10^{-9} mm Hg Vapor Density: Not available Refractive Index: Not available Solubility: Insoluble in water; slightly soluble in alcohol; soluble in benzene, toluene, xylene.

Log Partition Coefficient (octanol/water): 6.04

Photochemical Reactivity: Not available

Chemical Reactivity:

Hydrogenation with platinum oxide gives 4,5-dihydrobenzo(a) pyrene, 7, 8, 9, 10-tetrahydro(a)pyrene and perhydrobenzo(a) pyrene. On oxidation with chromic acid or ozone, B(a)P yields benzo(a)pyrene-1,6-quinone and benzo(a)pyrene-3,6-quineon; and on further oxidation, benzanthrone dicarboxylic anhydride. Electrophilic substitution occurs mainly in position 6. B(a)P oxidizes in benzene under the influence of light and air. When heated to decomposition, emits acrid smoke and irritating fumes.

Environmental Fate

Very strong adsorption onto suspended solids is the dominant transport process. Bioaccumulation is short-term; metabolism and microbial degradation are principal fates.

Source of Emissions

Production:

Produced in the United States by one company and distributed by several specialty companies in quantities from 100 mg to 5 g for research purposes. Although not produced in great quantities, it is a byproduct of combustion, and an estimated 1.8 million 1b per year is released from stationary sources--96 percent from coal refuse piles, outcrops, and abandoned coal mines; residential external combustion of bituminous coal; coke manufacture; and residential external combustion of anthracite coal. Has been detected in cigarette smoke at levels ranging from 0.2 to 12.2 μ g/100 cigarettes. Has been detected in foods at levels ranging from 0.1 to 50 ppb.

Uses:

Research purposes only

Tables E-1 and E-2 present emission factors and ambient concentrations of benzo(a)pyrene.

Storage:

In laboratory only

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Transportation:

Shipped only in small (less than 5 g) quantities

Cigarettes	2.5 µg/100 cigarettes
Automobile exhaust	0.05-0.08 mg/liter gasoline consumed
Fuel oil combustion (large furnace)	0.13 mg/ton fuel
Fuel oil combustion (small furnace)	10.6 mg/ton fuel
Space heaters (coal)	10 mg/10 ⁶ Btu input
Space heaters (gas)	0.2 mg/10 ⁶ Btu input
Refuse burning	11.0 g/m ³ of emitted gas
Power station (coal)	0.3 g/m ³ of emitted gas
Power station (gas)	0.1 g/m ³ of emitted gas
Automotive diesel	5.0 g/m ³ of emitted gas
Coke oven volatiles	35.0 g/m³ of emitted gas
Water spray-tower, asphaltic concrete	<100 ng/m³
Outlet of asphalt air-blowing process	<4,000 ng/m ³

TABLE E-1. EMISSION FACTORS FOR BENZO(A)PYRENE

Source: Verschueren, K. 1983.

		Benzo(a)pyrene, ng/m ³			
City		Spring	Summer	Fall	Winter
New York	-Commercial -Freeway -Residential	0.5-8.1 0.1-0.8 0.1-0.6	0.7-3.9 0.1-0.7 0.1-0.3	1.5-6.0 3.3-3.5 0.6-0.8	0.5-9.4 0.7-1.3 0.5-0.7
Detroit Atlanta	-Commercial -Freeway -Residential	7.2	- 4.0-6.0 0.2 1.6-4.0	- 3.4-7.3 - 12-15	5.0-17.0 9.2-13.7 0.9-1.8 2.1-9.9
Birmingh	am	6.3-18	6.1-10	20-74	23-34
Cincinna	ti	2.0-2.1	1.3-3.9	14-18	18-26
Detroit		3.4-12	4.1-6.0	18-20	16-31
Los Ange	les	0.4-0.8	0.4-1.2	1.2-13	1.1-6.6
Nashvill	е	2.1-9.0	1.4-6.6	30-55	26
New Orle	ans	2.6-5.6	2.0-4.1	3.6-3.9	2.6-6.0
Philadelphia		2.5-3.4	3.5-19	7.1-12	6.4-8.8
San Francisco		0.8-0.9	0.2-1.1	3.0-7.5	1.3-2.4
Pittsbur	gh	<u> </u>	0-23	2.9-37	8.2

TABLE E-2. BENZO(A)PYRENE CONTENT OF URBAN AIR

Source: Verschueren K. 1983.

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Disposition:

Benzo(a)Pyrene may be disposed of in an incinerator controlled by an afterburner and an alkaline scrubber. A flammable solvent must be added.

Sampling and Analytical Methods

- 1. NIOSH Method 186
 - a. Collection on a membrane filter.
 - b. Thin layer chromatographic separation.
 - c. Fluorometry.

Detection limit: 0.02 µg/m³

Possible interferences:

This method is highly selective for B(a)P, but is sensitive to variations in technique.

- 2. NIOSH Method 184
 - a. Collection on a filter.
 - b. Extraction.
 - c. Column chromatography.
 - d. Spectrophotometric measurement.

Detection limit: 4 mg/m³

Possible interferences: Any substance that hinders the gas chromatographic separation or that absorbs radiation at the same wavelength as the sample compounds may interfere.

- 3. NIOSH Method 183
 - a. Collection on a membrane filter.
 - b. Extraction.
 - c. GC separation.
 - d. Spectrophotometric separation.

Detection limit: 0.4 mg/m³ per 500-liter sample.

Possible interferences:

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Any compound that has about the same GC retention time will interfere.

- 4. NIOSH Method 206
 - a. Sampling with glass-fiber filter.
 - b. Extract ultrasonically.
 - c. Enrich and measure with high pressure chromatography.

Detection limit: 3.3 ng/m³

Possible interferences:

Any compound that is not retained in the silica column and absorbs light at 254 nm is measured in this procedure (eg. Fluorene + derivatives; polychloro-derivatives; di + tricyclic hydrocarbons). Most interfering compounds have low peak area/ μ g values.

Permissible Exposure Limits

OSHAACGIHTWANot establishedNot established

OSHA indirectly limits exposure by requiring that occupational exposure to coal tar pitch volatiles not exceed 0.2 mg/m^3 8 hr TWA.

The ACGIH lists benzo(a)pyrene as an industrial substance suspected of carcinogenic potential for man.

Human Toxicity

Acute Toxicity: High acute subcutaneous toxicity in rats only.

Chronic Toxicity:

Carcinogenesis--The activity of benzo(a)pyrene was first recognized decades ago, and since that time it has become a laboratory standard for the production of experimental tumors in animals that resemble human carcinomas. It ranks among the most potent animal carcinogens known and can produce tumors by single exposures to microgram quantities. It acts both at the site of application and at organs distant to the site of absorption. Its carcinogenicity has been demonstrated in nearly every tissue and species tested, regardless of the route of administration.

Mutagenicity--Benzo(a)pyrene gives positive results in nearly all mutagenicity test systems, including the Ames Salmonella assay, cultured Chinese hamster cells, the sister-chromated exchange test, and the induction of DNA repair synthesis.

Teratogenicity--Limited data available.

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a.

Chemical Name

1,3-Butadiene

CAS Number

106-99-0

Chemical Classification

Aliphatic hydrocarbon (unsaturated), alkadiene, olefin

Synonyms

Biethylene, biuinyl, butadieen, buta-1,3-dieen butadien, 1,3-butadien, butadiene, buta-1,3-diene, alpha-gamma-butadiene, divinyl, crythrene, NCI-C5602, pyrrolylene, vinylethylene

Physical/Chemical Properties

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Description:
     Colorless gas with mild aromatic odor; easily liquified.
Boiling Point:
     -4.41°C
Melting Point:
     -108.9°C
Molecular weight:
     54.1
Chemical Formula:
     H<sub>2</sub>C:CHHC:CH<sub>2</sub>
Vapor Pressure:
     17.65 psia at 0°C 1840 mm at 21°C
Vapor Density:
     1.87 (air = 1)
Refractive Index:
     N_{D}^{-25} = 1.4292
Solubility:
     Soluble in alcohol and ether; insoluble in water.
Log Partition Coefficient (octanol/water):
     1.99
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Photochemical Reactivity:

Estimated lifetime under photochemical smog conditions is less than one hour. Half-life for reaction (at 26.8° C) with HO· is 0.1 day and with O₃, 0.95 day.

Chemical Reactivity:

Very reactive. Dangerous when exposed to heat, flame, or powerful oxidizers. Reacts violently with phenol.

Environmental Fate

The most probable environmental fate is photooxidation in the troposphere. The high vapor pressure of 1,3-butadiene precludes transport from the troposphere although it is sufficiently soluble in water to be washed out of a polluted atmosphere in rainwater. However, rapid volatilization to the atmosphere from surface water is likely. There is no information indicating 1,3-butadiene bioaccumulations.

Source of Emissions

Production:

Ethylene coproduct (only method currently being used) Catalytic dehydrogenation of n-butene and n-butane (Houdry process) Oxidative dehydrogenation of n-butene

Uses:

Styrene-butadiene rubber and latex Polybutadiene Adiponitrile Chloroprene/neoprene ABS rubber Nitrile rubber Numerous polymers with styrene/acrylonitrile/vinylpyridine Other chemicals including captan; sulfolene;tetrahydrophthalic anhydride; 1-4-hexadiene; 1-5-hexadiene; 1,4-dichlorobutene; butadiene furfural cotriemer; and R-11 pesticide

Tables E-3 through E-8 present 1,3-butadiene production, consumption, and emission data.

Storage and Transportation:

Although butadiene is a gas at ambient temperatures, it is stored and shipped as a pressurized liquid. It is shipped by pipeline, rail tank car, tank truck, and marine vessel. There is an extensive butadiene pipeline network between petrochemical plants on the Texas Gulf; a substantial portion of the chemical is shipped by this method. Butadiene is a flammable gas and must be handled as such. It must be isolated from any oxidizing material. Electrical equipment with spark-resistant construction must be provided.

TABLE E-	3.	COMPANIES	PRODUCING	1.	.3-BUTADIENE
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Company	Location	Annual capacity, 10 ⁶ 1b
Atlantic Richfield Co. ARCO Chemical Co.	Channelview, TX	450
Dow Chemical U.S.A.	Freeport, TX	85
E.I. Du Pont de Nemours & Co., Inc. Conoco Chemicals Co.	Chocolate Bayou, TX	135
El Paso Products Co.	Corpus Christi, TX	220
Exxon Chemical Americas	Baton Rouge, LA	310
	Baytown, TX	240
Mobil Chemical Co.	Beaumont, TX	80
Shell Chemical Co.	Deer Park, TX	500
	Norco, LA	500
Standard Oil Co. (Indiana) Amoco Chemicals Corp.	Chocolate Bayou, TX	180
Tenneco, Inc. Texas Petrochemical Corp.	Houston, TX	600
Texaco Chemical Co.	Port Neches, TX	500
Union Carbide Corp.	Pensulas, PR	75
	Seadrift, TX	33
	Taft, LA	75
· ·	Texas City, TX	55
		Total 4, 038

Source: PEI Associates, Inc., 1985.

Product	Percentage of total consumption
Styrene-butadiene rubber (SBR)	44
Polybutadiene rubber (PBR)	19
Adiponitrile	11
Styrene-butadiene copolymer latexes	8
Neoprene	7
Acrylonitrile-butadiene-styrene (ABS) resins	6
Nitrile rubber (NBR)	3
Miscellaneous (pesticides, solvents, etc.)	2
Total	100

TABLE E-4. USE PATTERN FOR 1,3-BD

Source: Versar, Inc., 1984.

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Source	Uncontrolled emission ratio, kg/Mg	Control device or technique	Emission reduction, %	Controlled emission ratio, kg/Mg
Flue gas	0.06	None	0	0.06
Reactor vent (regeneration air)	5.50	Catalytic or thermal oxidation	9 2	0.44
Intermittent process emissions	0.50	Elevated flare	95	0.03
Storage and handling	0.10	None ^b		0.1
Secondary	0.15	None		0.15
Fugitive	5.20	Detection and repair of major leaks plus mechanical seals	90	0.52
Total	11.51		<u></u>	1.30

TABLE E-5. UNCONTROLLED AND CONTROLLED VOC EMISSIONS FROM BUTADIENE PRODUCTION BY DEHYDROGENATION OF n-BUTANE (HOUDRY PROCESS)

^a kg of VOC per Mg of butadiene produced.

^b Pressurized storage tanks vented to the process are considered to be normal conditions, not a separate emission control.

Source: Adapted from Standifer, 1980.

Source	Uncontrolled emission ratio, kg/Mg ^a	Control device or technique	Emission reduction, %	Controlled emission ratio, kg/Mg ^a
Flue gas	0.06	None	0	0.06
Absorption column vent	5.00	Catalytic or thermal oxidation	95	0.25
Intermittent process emissions	0.50	Elevated flare	95	0.03
Storage and handling	0.10	None ^b		0.10
Secondary	0.75	Reactor wastewater stripper-flare vented vapor	70	0.23
Fugitive	5.20	Detection and repair of major leaks plus mechanical seals	90	0.52
Total	11.61			1.19

TABLE E-6. UNCONTROLLED AND CONTROLLED VOC EMISSINS FROM BUTADIENE PRODUCTION BY OXIDATIVE DEHYDROGENATION OF <u>n</u>-BUTENES

^a kg of VOC per Mg of butadiene produced.

^b Pressurized storage tanks vented to the process are considered to be normal conditions, not a separate emission control.

Source: Adapted from Standifer, 1980.

Source	Uncontrolled emission ratio, kg/Mg	Control device or technique	Emission reduction, %	Controlled emission ratio, kg/Mg ^a
Flue gas	0.002	None		0.002
Hydrogenation catalyst regeneration vent	0.024	None		0.024
Methylacetylene column vent	2.100	Incineration or flare	95	0.105
Intermittent process emissions	0.250	Elevated flare	95	0.013
Storage and handling	0.100	None ^b		0.100
Secondary	0.150	None		0.150
Fugitive	2.500	Detection and repair of major leaks plus mechanical seals	90	0.250
Total	5.1			0.644

TABLE E-7. UNCONTROLLED AND CONTROLLED VOC EMISSIONS FROM BUTADIENE PRODUCTION BY EXTRACTION FROM ETHYLENE PLANT BY-PRODUCT STREAMS

^a kg of VOC per Mg of butadiene produced.

^b Pressurized storage tanks vented to the process are considered to be normal conditions, not a separate emission control.

Source: Adapted from Standifer, 1980.

Location	Average mean value	Maximum value	Comments
Houston, TX area	5.22 2.81	88.61 33.76	incl. tunnels excl. tunnels
Los Angeles, CA	24.23	88.39	
Riverside, CA	3.98	6.19	
Atlanta, GA	5.57		
Lincoln Tunnel, NY	20.11 1.64	24.09 2.71	in tunnel outside air
Columbus, OH	0.77	5.47	
Denver, CO	1.7	7.6	only one sample set
Jones State Forest, TX [*]	0.67	2.41	non-urban setting

TABLE E-8. 1,3-BUTADIENE MONITORING DATA

* 38 miles north of Houston, Texas.

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Source: Versar, Inc., 1984.

Disposition:

1,3-Butadiene may be disposed of by incineration.

Sampling and Analytical Methods

- 1. NIOSH Method S91
 - a. Adsorption on charcoal.
 - b. Desorption with carbon disulfide.
 - c. Gas chromatography with flame ionization detection.

Detection limit: 200 to 6600 mg/m³ (91-3000 ppm) with 1-liter sample.

Possible interferences:

High humidity can lower vapor trapping efficiency. Compounds that have the same retention time at the operating parameters mentioned above may interfere.

Permissible Exposure Limits

	<u> </u>	ACGIH
TWA STEL	1,000 ppm (2,200 mg/m³)	1,000 ppm (2,200 mg/m³) 1,250 ppm (2,750 mg/m³)

The ACGIH has listed 1,3-Butadiene for intended changes to delete the STEL, to change the TWA to 10 ppm (22 mg/m^3) and add a notation that 1,3-Butadiene is an industrial substance suspected of carcinogenic potential for man.

Human Toxicity

Acute Toxicity:

Vapors are irritating to eyes and mucous membranes. Inhalation of high concentrations can cause unconsciousness and death. If spilled on skin, can cause burns or frostbite (due to rapid vaporization). Human subjects tolerated 4,000 ppm for 6 hours with no apparent effects other than a slight irritation of the eyes. Tolerances to high exposures appear to develop following a single exposure. Human exposure of volunteers to 8,000 ppm for 8 hours caused eye and upper respiratory irritation.

Chronic Toxicity:

Chronic oncology studies completed for the National Toxicology Program have indicated that 1,3-butadiene is carcinogenic in both sexes of mice and rats at levels as low as 625 ppm.

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a.

Chemical Name

o-, m-, p-Cresol

CAS Number

95-48-7; 108-39-4; 106-44-5

Chemical Classification

Pheno1

Synonyms

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(2-,3-,4-,) cresol; (o-,m-,p-) cresylic acid; 1-hydroxy-(2-,3-,4-)
methylbenzene; (o-,m-,p-) hydroxytoluene; (2-,3-,4-) hydroxytoluene;
(0-,m-,p-) methylphenol; (o-,m-,p-) oxytoluene; phenol, 2-methyl-(9Cl)
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Physical/Chemical Properties

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Description:
      White crystals; phenol-like odor.
      Colorless to yellowish liquid; phenol-like odor.
      Crystalline mass; phenol-like odor
Boiling Point:
      191°C; 203°C; 202°C
Melting Point:
      30.9°C; 12°C; 35.3°C
Molecular Weight:
      108.1
\begin{array}{c} \text{Chemical Formula:} \\ \text{CH}_3\text{C}_6\text{H}_4\text{OH} \end{array}
Vapor Pressure:
      1 mm at 38.2°C; 1 mm at 52°C; 1 mm at 53°C
Vapor Density:
      3.72; 3.72; 3.72 (air = 1.0)
Refractive Index:
      N_{D}^{20} = 1.536; N_{D}^{20} = 1.544; N_{D}^{20} = 1.531
Solubility:
      Soluble in alcohol, ether, chloroform, and hot water
Log Partition Coefficient (octanol/water):
      3.40; 2.37; 2.35
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Photochemical Reactivity:

Reactivity toward OH• from 10 to 12 times butane. Reactivity toward O_3 is 10 percent of propylene. Major atmospheric precursor is toluene; less than 10 percent of cresols from toluene decay. o-Cresol reacts with oxidizing materials to yield quinones and benzenes; reacts in less than one day in air.

Chemical Reactivity:

Reacts violently with HNO_3 , oleum, and chlorosulfonic acid. Dangerous when heated to decomposition; emits highly toxic fumes. Can react vigorously with oxidizing materials.

Environmental Fate

Decomposes in a soil microflora in 1 day. An aqueous solution of cresol is destroyed by photooxidation.

Source of Emissions

Production: Coal tar (from coke and gas works) From toluene by sulfonation or oxidation

Uses:

Disinfectant Phenolic resins Tricresyl phosphate Ore flotation Textile scouring agent Organic intermediate, mfg. of salicylaldehyde Coumarin and herbicides Surfactant Synthetic food flavors (para isomer only)

Tables E-9 through E-20 present data on o-, m-, p-cresol production, consumption, and emissions.

Storage:

Should be stored in cool, dry, well-ventilated location, away from any area where the fire hazard may be acute. Should be protected against physical damage. Outside or detached storage is preferred; should be separated from oxidizing materials.

Transportation:

Shipped in glass bottles, 10- and 55-gallon metal drums, 55gallon metal barrels, tank trucks, tank cars, and tank barges.

Disposition:

Cresols may be disposed of by incineration.

Company	Location	Cresol isomer capacity, 10 ⁶ lb/yr	Cresol isomer produced, 10 ⁶ lb/yr	Geographic coordinates, latitude/longitude
o-Cresol Producers				
Continental Oil Fallek Ferro Koppers Merichem Stimson Total	Newark, NJ Tuscaloosa, AL Sante Fe Springs, CA Oil City, PA Houston, TX Anacartes, WA	7.7 9.6 4.5 5.4 15.1 4.5 46.8	5.0 6.0 3.0 3.0 10.0 3.0 30.0	40 43 34/74 07 26 33 11 00/87 34 50 33 56 30/118 04 18 41 29 30/79 43 20 29 45 36/95 10 48 48 28 31/122 32 48
n-Cresol Producer				
Sherwin Williams	Chicago, IL	N/A ^a	21.0	41 43 04/87 36 30
m-Cresol Producers				
Koppers Merichem	Oil City, PA Houston, TX	N/A N/A	0.75 0.75	41 29 30/79 43 20 29 45 36/95 10 48
Total			1.50	

TABLE E-9. CRESOLS ISOMER PRODUCERS

^aNot available

Source: Systems Applications, Inc., 1982.

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Company	Location	Tar acids capacity, 10 ⁶ 1b/yr	Cresols or cresylic acid produced, 10 ⁶ lb/yr	Geographic coordinates, latitude/longitude
Mixed Cresol Producers				
Continental Oil Fallek Ferro Koppers Merichem Stimson Total	Newark, NJ Tuscaloosa, AL Sante Fe Springs, CA Oil City, PA Houston, TX Anacartes, WA	50 20 30 35 100 30 265	6 2 4 4 12 4 32	40 43 34/74 07 26 33 11 00/87 34 50 33 56 30/118 04 18 41 29 30/79 43 20 29 45 36/95 10 48 48 28 31/122 32 48
Cresylic Acid Producers				
Continental Oil Crowley Tar Products Fallek Ferro Koppers Merichem Mobile, Oil Stimson	Newark, NJ Houston, TX Tuscaloosa, AL Santa Fe Springs, CA Follansbee, WV Houston, TX Beaumont, TX Anacortes, WA	50 30 20 30 35 100 10 30	9 5 3 5 6 17 2 5	40 43 34/74 07 26 29 43 50/95 14/20 33 11 00/87 34 50 33 56 30/118 04 18 40 23 10/80 35 07 29 45 36/95 10 48 34 04 14/94 03 40 48 28 31/122 32 48
Total		305	52	

TABLE E-10. MIXED CRESOLS AND CRESYLIC ACID PRODUCERS

Source: Systems Applications, Inc., 1980.

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TABLE E-11.	1978	END	USE	DISTRIBUTION	OF	CRESOL	ISOMERS,	CRESOLS,
			A	ND CRESYLIC AC	CID			

	Isomers, Cre or cresylic ac	sols, id used
	10 ⁶ lb/yr	%
o-Cresol Isomer		
2,6-ditert butyl-p-cresol (BHT) Antioxidants Export	15.0 10.0 5.0	50 33 17
Total	30.0	100
p-Cresol Isomer		
Phenolic resins Pesticides Export	5.5 5.0 10.5	26 24 50
Total	21.0	100
m-Cresol Isomer		
Pyrethroid pesticides	1.5	100
Mixed Cresols/Cresylic Acids Combined		
Tricresyl phosphate (TCP) Cresyl diphenol phosphate (CDF)} Phenolic resins Wire enamel solvent Pesticides Disinfectants/cleaning compound Ore flotation Miscellaneous other Export	31.0 20.0 20.0 8.0 3.0 3.0 7.0 5.0	32 21 21 8 3 3 7 5
Total	97.0	100

Source: Systems Applications, Inc., 1980.

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TABLE E-12. IDENTIFIED SOURCE LOCATIONS OF CRESOLS END-USERS

Company	Location	Production capacity, million lb/yr	Cresol usage, million lb/yr	Geographic coordinates, latitude/longitude
2,6 di-tert-buty-p-cresol (BHT) Products		<u>o-cresol Isomer</u>		
Ashland Koppers Shell Uniroyal	Fords, NJ Oil City, PA Martinez, CA Geismar, LA	12 9 10 5	5 4 4 2	40 31 20/74 20 50 41 29 30/79 43 20 38 00 05/122 05 40 30 13 30/91 00 15
Total		36	15	
<u>Pyrethroid Pesticide</u> <u>Producers</u> CPC International FMC Vertac	Lyndhurst, NJ Baltimore, MD West Helena, AR	<u>m-cresol Isomer</u> NA ^a NA NA	0.5 0.5 0.5	40 47 30/74 04 34 39 14 50/76 35 30 34 36 10/90 33 45
Total			1.5	
<u>Tricresyl Phosphate/Cresol</u> Diphenolphosphate Producers		Mixed cresols/ cresylic Acid		
FMC Stauffer	Nitro, WV Gallipolis Ferry, WV	60 50	20 11	38 25 33/81 50 05 38 46 40/82 10 54
Total		110	31	

^aNot available.

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Source: Systems Applications, Inc., 1982.

	Nationwi	Nationwide emissions		
Source	o-cresol	m-cresol	p-cresol	
o-m-p-Cresol production	75,000	3,750	105,000	
Mixed cresol production	24,800	34,400	20,800	
Cresylic acid production	3,525	39,950	41,125	
Phenolic resins production (isomer)	0	0	27,500	
BHT production	15,000	0	0	
Pyrethroid pesticide	0	750	0	
Antioxidants production	10,000	0	0	
Pesticides production	0	0	2,500	
Tricresyl phosphate production	2,120	5,800	4,900	
Phenolic resins	13,700	37,400	31,600	
Wire enamel solvent	2,740,000	7,480,000	6,320,000	
Pesticides	550	2,185	1,265	
Disinfectants/cleaning compounds	411,000	1,122,000	948,000	
Ore flotation agent	411,000	1,122,000	948,000	
Miscellaneous, other	1,000	2,600	2,200	
Coke ovens	796,080	1,104,240	667,680	
Total	4,503,775	10,995,075	9,120,570	

TABLE E-13. 1978 NATIONWIDE o-, m-, p-CRESOL EMISSIONS

Source: Systems Applications, Inc., 1982.

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TABLE E-14.	CRESOLS	PRODUCTION	AND	END-USE	EMISSION	FACTORS
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	16 10	lb lost per lb produced (used)						
Source	Process	Storage	Fugitive	Total	Deriva- tion ^a			
Mixed cresol production	0.00190	0.00020	0.00040	0.00250	В			
Cresylic acid production	0.00190	0.00020	0.00040	0.00250	В			
p-Cresol production	0.0039	0.00030	0.00080	0.00500	D			
BHT/antioxidants	0.0008	0.0001	0.0001	0.001	D			
Phenolic resins	0.00400	0.0005	0.0005	0.00500	D			
Pesticides	0.00040	0.00005	0.00005	0.00050	С			
Pyrethroid pesticides	0.00040	0.00005	0.00005	0.00050	D			
TCP production	0.00035	0.00005	0.00010	0.0005	С			
Miscellaneous, other				0.001 ^b				

^aBasis: A - site visit data, B - state files, C - published data, D -Hydroscience estimate

^bBased on a weighted average all of cresol uses.

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Source: Systems Applications, Inc., 1982

		Emissions lb/yr				otal missions
Company	Location	Process	Storage	Fugitive	.1b/yr	g/sec
	0-Cr	resols Produc	ers			
Continental Oil	Newark, NJ	9,500	1,000	2,000	12,500	0.18
Fallek	Tuscaloosa, AL	11,400	1,200	2,400	15,000	0.22
Ferro	Santa Fe Springs, CA	5,700	600	1,200	7,500	0.11
Koppers	Oil City, PA	5,700	600	1,200	7,500	0.11
Merichem	Houston, TX	19,000	2,000	4,000	25,000	0.36
Stimson	Anacortes, WA	5,700	600	1,200	7,500	0.11
Total		57,000	6,000	12,000	75,000	
	p-(resol Produc	er			
Sherwin Williams	Chicago, IL	81,900	6,300	16,800	105,000	1.51
	m-Cr	resol Produce	ers			
Koppers	Oil City, PA	1,425	150	300	1,875	0.03
Merichem	Houston, TX	1,425	150	300	1,875	0.03
Total		2,850	300	600	3,750	

TABLE E-15. CRESOL ISOMER EMISSIONS FROM CRESOL, ISOMER PRODUCERS

Source: Systems Applications, Inc., 1982.

		Emission lb/yr			Total cresol emissions		
Company	Location	Process	Storage	Fugitive	lb/yr	g/sec	
Continental Oil	Newark, NJ	11,400	1,200	2,400	15,000	0.22	
Fallek	Tuscaloosa, AL	3,800	400	800	5,000	0.07	
Ferro	Santa Fe Springs, CA	7,600	800	1,600	10,000	0.14	
Koppers	Oil City, PA	7,600	800	1,600	10,000	0.14	
Merichem	Houston, TX	22,800	2,400	4,800	30,000	0.43	
Stimson	Anacortes, WA	7,600	800	1,600	10,000	0.14	
Total		60,800	6,400	12,800	80,000		

TABLE E-16. CRESOL EMISSIONS FROM MIXED, CRESOL, CRESYLIC ACID PRODUCERS

Cresylic Acid Producers

Continental Oil	Newark, NJ	17,100	1,800	3,600	22,500	0.32
Fallek	Tuscaloosa, AL	5,700	600	1,200	7,500	0.11
Ferro	Santa Fe Springs, CA	9,500	1,000	2,000	12,500	0.18
Koppers	Follansbee, WV	11,400	1,200	2,400	15,000	0.22
Merichem	Houston, TX	32,300	3,400	6,800	42,500	0.61
Mobil Oil	Beachmont, TX	3,800	400	800	5,000	0.07
Stimson Lumber	Anacortes, WA	9,500	1,000	2,000	12,500	0.18
Total		89,300	9,400	18,800	117,500	

Source: System Applications, Inc., 1982.

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		Emi	ssions 1b/	yr	To cresol en	otal nissions
Company	Location	Process	Storage	Fugitive	1b/yr	g/sec
	o-Cre	sols Produc	ers		• <u>••••</u> •••••••••••••••••••••••••••••••	
2-6-Di-tert-buty-p-cres (BHT) producers	01					
Ashland Koppers Shell Uniroyal	Fords, NJ Oil City, PA Martinez, CA Geismar, LA	4,000 3,200 3,200 1,600	500 400 400 200	500 400 400 200	5,000 4,000 4,000 2,000	0.07 0.06 0.06 0.03
Total		12,000	1,500	1,500	15,000	
	m-Cr	esol Produc	er			
Pyrethroid Pesticide Producers						
CPC International FMC Vertac	Lyndhurst, NJ Baltimore, MD West Helena, AR	200 200 200	25 25 25	25 25 25	250 250 250	0.004 0.004 0.004
Total		600	75	75	750	
	Mixed Cre	sols/Cresyl	ic Acid			
Tricresyl phosphate/cre diphenylphosphate prod	syl ucers					
FMC <u>Stauffer</u> Total	Nitro, WV Gallipolis Ferry, WV	7,000 3,850 10,850	1,000 550 1,550	2,000 1,100 3,100	10,000 5,500 15,500	0.14 0.08

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TABLE E-17. CRESOL EMISSIONS FROM CRESOL USERS

Source: Systems Applications, Inc., 1982

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Region	Number of sites	o-Cresol emissions lb/yr	m-Cresol emissions lb/yr	p-Cresol emissions lb/yr	Total cresol emissions lb/yr
New England	0	0	0	0	0
Middle Atlantic	15	195,750	271,500	164,175	631,425
East North Central	25	326,250	452,500	273,625	1,052,375
West North Central	3	39,150	54,300	32,835	126,285
South Atlantic	4	52,200	72,400	43,780	168,380
East South Central	9	117,450	162,900	98,505	378,855
West South Central	2	26,100	36,200	21,890	84,190
Mountain	2	26,100	36,200	21,890	84,190
Pacific	1	13,050	18,100	10,945	42,095
Total	61	796,050	1,104,100	667,645	2,567,795

TABLE E-18. CRESOL ISOMER EMISSIONS FROM COKE OVEN OPERATION^a

^aBasis: 107 billion 1b coke produced; 0.000024 1b cresols emitted/1b coke produced; cresol composition - 25 percent p-cresol, 31 percent o-cresol, and 43 percent m-cresol in mixed cresols emitted.

Source: Systems Applications, Inc., 1982.
Region	Number of sites	o-Cresol emissions lb/yr	p-Cresol emissions lb/yr	m-Cresol emissions lb/yr
New England	46	79,975	184,465	218,325
Middle Atlantic	339	589,380	1,359,440	1,608,960
East North Central	370	643,275	1,483,755	1,756,090
West North Central	84	146,040	336,855	398, 680
South Atlantic	174	302,510	697,765	825,835
East South Central	44	76,500	176,445	208,830
West South Central	87	151,255	348,885	412,920
Mountain	258	448,555	1,034,620	1,224,520
Pacific	174	302,510	697,765	825,840
Total	1,576	2,740,000	6,319,995	7,480,000

TABLE E-19. CRESOL ISOMER EMISSIONS FROM MIXED CRESOLS/CRESYLIC ACID USED AS WIRE ENAMEL SOLVENT

Source: Systems Applications, Inc., 1982.

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Region	Number of sites	o-Cresol emissions lb/yr	p-Cresol emissions lb/yr	m-Cresol emissions lb/yr
New England	6	4,382	11,957	10,103
Middle Atlantic	38	27,750	75,729	63,987
East North Central	85	62,075	169,392	143,128
West North Central	145	105,890	288,964	244,159
South Atlantic	62	45,275	123,557	104,399
East South Central	40	29,211	79,714	67,354
West South Central	21	15,336	41,850	35,361
Mountain	144	105,161	286,971	242,475
Pacific	22	16,066	43,843	37,045
Total	563	411,000	1,122,000	984,000

TABLE E-20. CRESOL ISOMER EMISSIONS FROM MIXED CRESOLS/CRESYLIC ACID USED AS AN ORE FLOTATION AGENT

Source: Systems Applications, Inc., 1982.

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Sampling and Analytical Methods

- 1. NIOSH Method 2001
 - a. Absorption on silica gel.
 - b. Desorption with acetone.
 - c. Gas chromatography.
- Detection limit: 5 to 60 mg/m³ in a 20-liter sample

Possible interferences: High humidity can cause lower vapor trapping efficiency. Compounds with the same retention time may cause interference.

Permissible Exposure Limits

	OSHA (skin)	ACGIH (skin)	NIOSH (skin)
TWA	5 ppm (22 mg/m ³)	5 ppm (22 mg/m ³)	2.3 ppm (10 mg/m ³)
Odor perception	0.022 mg/m ³		

Human Toxicity

Acute Toxicity:

Cresol vapors or liquids are readily absorbed through the skin or any mucous membrane, which may cause acute and chronic poisoning. Skin contact with concentrated solutions can result in severe burns. Cresols are not sufficiently volatile to constitute a respiratory hazard under normal conditions. Systematic poisoning has rarely been reported, but it is possible that adsorption may result in damage to the kidneys, liver, and nervous systems.

Chronic Toxicity:

No reports of epidemiologic studies of worker exposures to cresol were found. No investigations of the mutagenic or teratogenic potential of cresol were found. The cresol isomers promoted DMBA-induced papillomas in mice, but no carcinomas were produced.

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a.

Chemical Name

p-Dichlorobenzene

CAS Number

106-46-7

Chemical Classification

Chlorinated aromatic hydrocarbon.

Synonyms

P-chlorophenyl chloride; P-dichlorobenzeen; 1,4-dichloorbenzeen; P-dichlorbenzol; 1,4-dichlorbenzol; Di-chloricide; P-dichlorobenzene; 1,4-dichlorobenzene; p-dichlorobenzol; dichlorobenzene, para, solid; 1,4-dichlorobenzene; p-dichlorobenzene; evola; NCL-C54955; paracide; paracrystals; paradi; paradichlorobenzene; paradichlorobenzol; paradon; paramoth; paranuggets; parazene; PDB; PDCB; persia-perazol; santochlor.

Physical/Chemical Properties

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Description:
     White crystals; volatile (sublimes readily); penetrating odor.
Boiling Point:
     173.7°C
Melting Point:
     53°C
Molecular weight:
     147.0
Chemical Formula:
     C_6H_4Cl_2
Vapor Pressure:
     10 mm at 54.8°C
Vapor Density:
     5.08 (air = 1)
Refractive Index:
     N_D^{20} = 1.5285
Solubility:
     Soluble in alcohol, benzene, and ether. Insoluble in water.
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Log Partition Coefficient (octanol/water): 3.39

Photochemical Reactivity:

Reactivity toward HO+ is 50 percent of butane. Reactivity toward O_3 is 5 percent of propylene. No major atmospheric precursors.

Chemical Reactivity:

Can react vigorously with oxidizing materials. When heated to decomposition or on contact with acid or acid fumes, will evolve toxic chloride fumes.

Environmental Fate

Volatilizes at a relatively rapid rate; half-life less than 12 hours. Bioaccumulates more than chlorobenzene; too resistant to biodegradation to compete with volatilization. Oxidized by hydroxy radicals in atmosphere.

Source of Emissions

Production/processing: Chlorination of monochlorobenzene

Uses:

Moth repellant General insecticide Germicide Space odorant Manufacture of 2,5-dichloroaniline Dyes Intermediates Pharmaceuticals Agriculture (fumigating soil)

Tables E-21 through E-25 and Figure E-1 present p-dichlorobenzene production, consumption, and emission data.

Storage:

Should be protected against physical damage and stored in cool, dry, well-ventilated place, away from any area where the fire hazard may be acute (outside or detached storage is pre-ferred), separate from oxidizing materials.

Transportation:

Should be shipped in 5-, 10-, 55-, and 110-gallon drums or tank cars.

Disposition:

P-dichlorobenzene may be disposed of by incineration, preferably after mixing with another combustible fuel. Care must be exercised to assure complete consumption to prevent the formation of phosgene. An acid scrubber is necessary to remove the halo acids produced.

Source	Location	1978 Estimated production, ^a 10 ⁶ 1b/yr	1978 Estimated capacity, 10 ⁶ lb/yr	Geographic coordinates latitude/longitude
Dow _	Midland, MI	9	30	43 35 28/84 13 08
Monsanto	Sauget, IL	4	12	38 35 31/90 10 11
PPG	New Martinsville, WV	13	40	39 47 22/80 51 27
Standard Chlorine	Delaware City, DE	24	75	33 33 54/75 38 47
Specialty Organics ^b	Irwindale, CA	1	2	34 06 30/117 55 48
Montrose	Henderson, NV	2	7	36 03 32/114 58 34
ICC	Niagara Falls, NY	2	8	43 03 33/79 00 55
Total		55	174	

TABLE E-21. p-DICHLOROBENZENE PRODUCERS

^aTotal production was distributed per site based on capacity.

^bProcesses dichlorobenzenes from Montrose.

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Source: Systems Applications, Inc. 1980.

End-Use	Volume, million lb/yr	Usage, %		
Space deodorant	27.5	50		
Moth control	22	40		
Pesticide intermediate	5.5	10		
TOTAL	55	100		

TABLE E-22. p-DICHLOROBENZENE END-USE DISTRIBUTION 1978

Source: Systems Applications, Inc., 1980.

TABLE E-23. 1978 NATIONWIDE EMISSIONS OF p-DICHLOROBENZENE

Source	Nationwide emissions, lb/year
Production	398,200
Space deodorant	27,500,000
Moth control	22,000,000
Pesticide intermediate	2,750
TOTAL	49,900,950

Source: Systems Applications, Inc., 1980.

a.

		E	missions, 1	Total emissions		
Source	Location	Process	Storage	Fugitive	lb/year	g/s
Dow	Midland, MI	52,290	3,690	9,180	65,160	0.94
Monsanto	Sauget, IL	23,240	1,640	4,080	28,960	0.42
PPG	New Martinsville, WV	75,530	5,330	13,260	94,120	1.35
Standard Chlorine	Delaware City, DE	139,440	9,840	24,480	173,760	2.50
Specialty Organics	Irwindale, CA	5,810	410	1,020	7,240	0.10
Montrose	Henderson, NV	11,620	820	2,040	14,480	0.21
ICC	Niagara Falls, NY	11,620	820	2,040	14 ,480	0.21
Total		319,550	22,550	56,100	398,200	

TABLE E-24. P-DICHLOROBENZENE EMISSIONS FROM PRODUCTION SITES

Source: Systems Applications, Inc. 1980.

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			C+au	Emissions, gm/s		/s
Company	Site	Latitude/longitude	star	Process	Storage	Fugitive
Dow	Midland, MI	43 35 28/084 13 08	14845	0.752976	0.053136	0.132192
Monsanto	Sauget, IL	38 35 31/090 10 11	13994	0.334656	0.023616	0.058752
PPG	New Martinsville, WV	39 47 22/080 51 27	13736	1.087632	0.076752	0.190944
Standard Chlorine	Delaware City, DE	39 33 54/075 38 47	94741	2.007936	0.141696	0.352512
Specialty Organics	Irwindale, CA	36 06 30/117 55 48	23215	0.083664	0.005904	0.014688
Montrose	Henderson, NV	36 03 32/114 58 34	23112	0.167328	0.011808	0.029376
100	Niagara Falls, NY	43 03 33/079 00 55	14747	0.167328	0.011828	0.029376

TABLE E-25. EMISSIONS AND METEROLOGICAL STATIONS OF SPECIFIC POINT SOURCES OF p-DICHLOROBENZENE

Source: Systems Applications, Inc. 1982.

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Figure E-1. Specific point sources of p-Dichlorobenzene emissions. Source: Systems Applications, Inc. 1980

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Sampling and Analytical Methods

1. NIOSH Method S281 a. Adsorption on charcoal. b. Desorption with carbon disulfide. c. Gas chromatography. Detection limit: 75 to 1350 mg/m³ (17.5-300 ppm); 170-liter sample. Possible interferences: None identified. ... Method B (Appendix A): C_2-C_{18} hydrocarbons and other 2. nonpolar organics with a boiling point of 100° to 175°C a. Whole air collection in canister. b. Cryogenic concentration. c. Gas chromatography/flame ionization detection. Detection limit: 0.1 ppb per 100-ml sample. Possible interferences: Storage times greater than a week are not recommended. 3. Method C (Appendix A): C_6-C_{12} hydrocarbons and other nonpolar organics with a boiling point between 60° and 200°C a. Adsorption on Tenax (resin adsorption/solvent desorption may be used). b. Thermal desorption. c. Gas chromatography/mass spectrometry analysis (gas chromatography/electron capture detection or photoionization detection may also be used). Detection limit: 1 to 200 ppt per 20-liter sample. Possible interferences: Blank levels usually limit sensitivity artifacts due to reactive components $(0_3, NO_y)$. Sample can be analyzed only once. 4. Method D (Appendix A): C_6-C_{12} hydrocarbons and other nonpolar organics with a boiling point of 60° to 200°C a. Adsorption on Tenax (resin adsorption/solvent desorption may be used). b. Thermal desorption into canisters. Gas chromatography/flame ionization detection or gas c. chromatography/mass spectrometry analysis. (Gas chromatography/electron capture detection or photoionization detection also may be used.)

a.

Detection limit: 0.01 to 1 ppb per 20-liter sample.

Possible interferences: Blanks and artifact problems, as in Method C.

Permissible Exposure Limits

	OSHA	ACGIH
TWA	75 ppm (450 mg/m ³)	75 ppm (450 mg/m ³)
STEL		110 ppm (675 mg/m³)

Human Toxicity

Acute Toxocity: Toxicity is high orally; moderate via intraperitoneal or inhalation. Has been reported to cause liver injury in humans.

Chronic Toxicity:

Carcinogenic determination in both animals and humans is indefinite. Currently tested by the National Toxicology Program for carcinogenesis bioassay as of January 1983.

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Chemical Name

Dimethylnitrosamine

CAS Number

62-75-9

Chemical Classification

Nitrosamine

Synonyms

Dimethylnitrosamin; dimethylnitrosamine; N,N-dimethyl-nitrosamine; dimethylnitrosoamine; DMN; DMNA; N₁-methyl-N-nitrosomethanamine; NDMA; nitrosodimethylamine; N-nitrosodimethylamine.

Physical/Chemical Properties

Description: Yellow liquid Boiling Point: 152°C Melting Point: Not available Molecular Weight: 74.1 Chemical Formula: (CH3)2N20 Vapor Pressure: Not available Vapor Density: 2.56 (air = 1) Refractive Index: $N_{D}^{20} = 1.4358$ Solubility: Soluble in water, alcohol and ether. Log Partition Coefficient (octanol/water): Not available Photochemical Reactivity: Photochemically reactive

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Chemical Reactivity:

Strong oxidants (peracids) oxidize it to the corresponding nitrosamine; can be reduced to the corresponding hydrazine and/or amine. Relatively resistant to hydrolysis but can be easily split by hydrogen bromide in acetic acid. When heated, it dampens to emit NO.

Environmental Fate

Biodegradation of 0.01 mg/liter is 100 percent in 15 days in both freshwater and seawater.

Source of Emissions

Production/processing:

From sodium nitrile and dimethyl amine hyperchloride.

Uses:

Prior to April 1, 1976, NDMA was used in the United States as an intermediate in the production of 1,1-dimethyl hydrazine, a storable liquid rocket fuel. No evidence of present use except for research purposes.

Storage:

Mixture containing 1 percent or more NDMA must be maintained in isolated or closed systems. Entrance to regulated area posted "Cancer-Suspect Agent Exposed in This Area. Impervious Suit Including Gloves, Boots, and Air-Supplied Hood Required at All Times. Authorized Personnel Only."

Transportation:

Certain procedures must be followed in movement of material and in case of accidental spills and emergencies. OSHA Standards, Subpart Z, Section 1910.1016.

Disposition:

Dimethyl nitrosamine may be disposed of by pouring over soda ash, neutralizing with HCl.

Sampling and Analytical Methods

- 1. NIOSH Method 252
 - a. Tenax GC absorption.
 - b. Thermal desorption with the purge.
 - c. Capillary gas-liquid chromatography.
 - d. Mass spectrometry.

Detection limit: 0.5 ppt to 10 ppb per 150-liter sample. Possible interferences:

Materials having background ions of m/e 74 ($C_2H_8N_3$, $C_2H_4NO_2$, $C_6H_6N_2O$, C_3H_3Cl , C_3H_6S , $C_3H_6O_2$, or $C_3H_{10}N_2$) if at the same retention time as DMN.

- 2. NIOSH Method 299
 - a. Adsorption on Tenax-GC.
 - b. Thermal adsorption.
 - c. GC-NPD.

Detection limit: 2-1000 gm/m³ per 5-liter sample.

Possible interferences:

Any compound that has the same retention time as the analyte is a potential interferent. Process is most selective for nitrogen or phosphorous containing compounds.

- 3. Method M (Appendix A)
 - a. Adsorption on Thermosorb N.
 - b. Thermal desorption.
 - c. Gas chromatography/mass spectrometry or thermal energy detectors (in relatively "clear" environments, a gas chromatography/nitrogen phosphorus detection approach may be used).

Detection limit: 25 mg/m³ per 200-liter sample.

Possible interferences:

Thermal energy analyzer is a nitrosamine-specific detector and is rather expensive. Gas chromatography/nitrogen phosphorus detection may be a less expensive alternative in many situations.

Permissible Exposure Limits

	OSHA	ACGIH
TWA	Not established	Not established

Specific regulations regarding use of a regulated area and labeling requirements, are presented in Section 1910.1016 of Subpart Z of the Occupational Safety and Health Standards. The ACGIH has listed dimethyl nitrosamine as an industrial substance suspected of carcinogenic potential for man (skin).

Human Toxicity

Acute Toxicity: High oral, inhalation, intraperitoneal, and subcutaneous toxicity. Has caused fatal liver disease in humans.

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Chronic Toxicity:

There is sufficient evidence to substantiate a carcinogenic effect in many experimental animal species. Similarities in its metabolism by human and rodent tissues have been demonstrated. Although no epidemiological data are available, dimethylnitrosamine should be regarded (for practical purposes) as if it were carcinogenic to humans.

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Chemical Name

Ethylene dichloride

CAS Number

107-06-2

Chemical Classification

Chlorinated hydrocarbon (unsaturated)

Synonyms

Aethylenchlorid; 1,2-bichloroethane; bichorure d'ethylene; berer sol; brocide; chlorure d'ethylene; cloruro di ethene; destruxol borer-sol; 1,2-dichloroethaan; 1,2-dichlor-aethan; dichloremulsion; 1,2-dichlorethane; dichlor-mulsion; dichloro-1,2-ethane; alphabeta-dichloroethane; sym-dichloroethane; 1,2-dichloroethane; dichloroethylene; 1,2-dichloroetano; Dutch liquid; Dutch oil; EDC; Ent 1,656; ethane dichloride; ethyleendichloride; ethylene chloride; ethylene dichloride; ethylene dichloride (DOT); 1,2-ethylene dichloride; freon 150; glycol dichloride; NCI-00511.

Physical/Chemical Properties

Description: Colorless oily liquid; chloroform-like odor; sweet taste Boiling Point: 83.5°C Melting Point: -35.5°C Molecular Weight: 100.0 Chemical Formula: C1CH, CH, C1 Vapor Pressure: 100 mm at 29.4°C Vapor Density: 3.35 (air = 1) **Refractive Index:** $N_D^{20} = 1.445$ Solubility: Miscible with most common solvents; slightly soluble in water.

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Log Partition Coefficient (octanol/water): 1.48

Photochemical Reactivity: Evaporates rapidly from water to the atmosphere, where it is destroyed by photooxidation.

Chemical Reactivity: Stable to water, acids, and bases, and also resists oxidation. Incompatible with dinitrogen tetroxide, metals.

Environmental Fate

Due to a high vapor pressure, volatilization to the atmosphere is rapid and is the major transport process. Photooxidation in the troposphere may be a predominant fate. Photooxidation in the aquatic environment occurs at a slow rate.

Source of Emissions

Production/processing: Action of chlorine on ethylene with subsequent distillation, with metalic catalyst. Reaction of acetylene and HCl.

Uses:

Vinyl chloride solvent Lead scavenger in antiknock gasoline Paint, varnish, and finish remover Metal degreasing Soaps and scouring compounds Wetting and penetrating agents Organic synthesis Ore flotation

Tables E-26 through E-30 present ethylene dichloride production, consumption, and emission data.

Storage and Transportation:

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Protect against physical damage. Outside or detached storage is preferable. Inside storage should be in a standard flammable-liquids storage room or cabinet, separate from oxidizing materials. Shipped by 1-gallon cans, 5- to 55-gallon metal drums, tank cars, and tank barges.

Disposition:

Ethylene dichloride may be disposed of by incineration, preferably after mixing with another combustible fuel. Care must be exercised to assure complete combustion to prevent formation of phosgene. An acid scrubber is necessary to remove the halo acids produced. Alternatively, ethylene dichloride may be recovered from process off-gases.

Producer	Location	Capacity	VCM	1,1,1- TCE	TCE	PCE	EA	VDCM	Scavenger
Borden Chemical	Geismar, LA		224						
Conoco Chemical	Lake Charles, LA	524	525						
Diamond Shamrock	Deer Park, TX	145			17	45			
Diamond Shamrock	La Porte, TX	719	749						
Dow Chemical	Freeport, TX	726	150	167	51	0 ^b	60	45 ^C	
Dow Chemical	Oyster Creek, TX	499	525			o ^b			
Dow Chemical	Pittsburg, CA					0 ^b			
Dow Chemical	Plaquemine, LA	953	936	112				45 ^C	
Du Pont	Antioch, CA								20 ^C
Du Pont	Corpus Christi, TX				0 ^b				
Du Pont	Deepwater, NJ							}	20 ^C
Ethyl Corporation	Baton Rouge, LA	318	248		15	14		20 ^C	
Ethyl Corporation	Houston, TX	118							20 ^C
B. F. Goodrich	Calvert City, KY	454	749						
Houston Chemical	Beaumont, TX								15 ^C
ICI America ^a	Baton Rouge, LA	318	224					1	
Monochem	Geismar, LA		0 ^b						

TABLE E-26. ETHYLENE DICHLORIDE PRODUCERS AND MAJOR CONSUMERS (January 1, 1979, production capacities in thousands of metric tons)

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TABLE E-26 (continued)

Producer	Location	Capacity	VCM	1,1,1- TCE	TCE	PCE	EA	VDCM	Scavenger
Malco Chemical	Freeport, TX								5 ^C
PPG Industries	Lake Charles, TX	544	229	130	68	54		30 ^C	
PPG Industries	Guayanilla, PR	379	375						
Shell Chemical	Deer Park, TX	635	629						
Shell Chemical	Morco, LA	544	525						
Stauffer Chemical	Carson, CA	154	130						
Stauffer Chemical	Louisville, KY					0 ^b			
Union Carbide	Taft, LA	68					70		
Union Carbide	Texas City, TX	68	ļ				60		
Vulcan Chemical	Geismar, LA	150		0 ^b		41			
Vulcan Chemical	Wichita, KS					0 ^b			
Total		7,316	6,218	409	151	154	190	140	80

^aPlant was purchased from Allied Chemical in September 1978.

^bProcess does not use EDC as a feedstock

^CRough order estimates.

Source: SRI International, 1979.

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	Emissions, 1,000 mt/yr
EDC production	
Fugitive Storage Direct chlorination Oxychlorination	5.2 14.5 6.3 17.9
Subtotal	43.9
Production in using EDC as Feedstock	
VCM 1,1,1-TCE TCE PCE EA VDCM Lead scavenger	1.1 0.4 0.2 0.3 0.3 0.2 0.2
Subtotal	2.7
Automobile Gasoline	
Service stations Auto emissions	0.1 1.2
Subtotal	1.3
Other	
Dispersive uses Transportation Waste disposal ^a	5.0 0.0 0.0
Total	52.9

TABLE E-27. ESTIMATED ATMOSPHERIC EMISSIONS OF ETHYLENE DICHLORIDE FOR 1977

^aNot included. Rough order estimates place these emissions at much less than 2,400 mt/yr for transportation and much less than 29,000 mt/yr for waste disposal.

Source: SRI International, 1979.

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		Production ^a					
Plant	Location	10 ³ mt/yr	Fugitive	Storage	Direct	Oxychlori nation	- Total
Conoco	Lake Charles, LA	372	11.8	33.0	12.8	12.6	70.2
Diamond	Deer Park, TX	103	3.3	9.1	2.6	1.9	16.9
Diamond	La Porte, TX	510	16.2	45.3	17.8	15.8	95.1
Dow	Freeport, TX	515	16.3	45.7	20.5	67.3	149.8
Dow	Oyster Creek, TX	354	11.2	31.4	12.4	0.0	55.0
Dow	Plaquemine, LA	678	21.5	60.1	24.4	99.5	205.5
Ethy1	Baton Rouge, LA	226	7.2	20.1	8.3	43.7	79.3
Ethy1	Houston, TX	84	2.7	7.5	5.9	0.0	16.1
Goodrich	Calvert City, KY	322	10.2	28.6	7.5	26.6	72.9
ICI America	Baton Rouge, LA	226	7.2	20.1	10.5	70.6	108.4
PPG	Lake Charles, LA	386	12.3	34.3	20.8	0.0	67.4
PPG	Guayanilla, PR	269	8.5	23.9	9.4	41.4	83.2
She11	Deer Park, TX	451	14.3	40.0	20.8	27.1	102.2
Shell	Morco, LA	386	12.3	34.3	13.5	59.4	119.5
Stauffer	Carson, CA	109	3.5	9.7	5.3	19.6	38.1
Union Carbide	Taft, LA	48	1.5	4.3	3.4	0.0	9.2
Union Carbide	Texas City, TX	48	1.5	4.3	3.4	0.0	9.2
Vulcan	Geismar, LA	107	3.4	9.5	0.0	80.8	93.7
Total		5,194	164.9	461.2	199.3	566.3	1,391.7

TABLE E-28. ESTIMATED ATMOSPHERIC EMISSIONS FROM ETHYLENE DICHLORIDE PRODUCTION FACILITIES

^aAssumed to be 71 percent of production capacity.

Souce: SRI International, 1979.

TABLE E-29.	ESTIMATED EDC	ATMOSPHERIC	EMISSIONS	FOR	PLANTS	THAT	USE	ETHYLENE	DICHLORIDE
		A	S A FEEDSTO)CK					
			(g/s)						

Producer	Location	VCM	1,1,1- TCE	TCE	PCE	EA	VDCM	Lead scavenger	Total
Borden Chemical	Geismar, LA	1.2							1.2
Conoco Chemical -	Lake Charles, LA	2.9							2.9
Diamond Shamrock	Deer Park, TX			0.7	1.6				2.3
Diamond Shamrock	La Porte, TX	4.1			÷				4.1
Dow Chemical	Freeport, TX	0.8	5.6	2.0		2.7	2.3		13.4
Dow Chemical	Oyster Creek, TX	2.9							2.9
Dow Chemical	Plaquemine, LA	5.1	3.7						8.8
Du Pont	Antioch, CA						2.3	1.1	3.4
Du Pont	Deepwater, NJ							1.1	1.1
Ethyl Corporation	Baton Rouge, LA	1.4		0.6	0.5			1.1	3.6
Ethyl Corporation	Houston, TX							1.1	1.1
B. F. Goodrich	Calvert City, KY	4.1							4.1
Houston Chemical	Beaumont, TX							0.9	0.9
ICI America	Baton Rouge, LA	1.2			1				1.2
Malco Chemical	Freeport, TX							0.3	0.3
PPG Industries	Lake Charles, TX	1.3	4.3	2.7	1.9)	1.5		11.7
PPG Industries	Guayanilla, PR	2.1							2.1

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TABLE E-29 (continued)

Producer	Location	VCM	1,1,1- TCE	TCE	PCE	EA	VDCM	Lead scavenger	Total
Shell Chemical	Deer Park, TX	3.4							3.4
Shell Chemical	Morco, LA	2.9							2.9
Stauffer Chemical	Carson, CA	0.7							0.7
Union Carbide	Taft, LA					3.2			3.2
Union Carbide	Texas City, TX					2.7			2.7
Vulcan Chemical	Geismar, LA			Į	1.5				1.5
Total	L	34.1	13.6	6.0	5.5	8.6	6.1	5.6	79.5

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Source: SRI International, 1979.

Detection limit: 0.01 to 1 ppb per 20-liter sample

Possible interferences: Blanks and artifact problems as in Method C.

Permissible Exposure Limits

OSHA		ACGIH	NIOSH			
TWA	50 ppm	10 ppm (40 mg/m ³)	$1 \text{ ppm} (4 \text{ mg/m}^3)$			
STEL		15 ppm (60 mg/m³)				
Ceiling	100 ppm		2 ppm (8 mg/m³)			
Peak	200 ppm (5 min in 3 h)					

The ACGIH has listed ethylene dichloride for intended changes to delete the STEL.

Human Toxicity

Acute Toxicity:

Most injurious exposures are acute episodes occurring because of accidental or industrial exposure. Ingestion of 20 to 50 ml is often fatal within a few days. Blood disorders appear characteristic of injection, and clotting difficulties are the most common. Death most often is attributed to circulatory and respiratory failure with varying degrees of liver and kidney damage. The effect of acute exposure to DCE by skin absorption and inhalation is similar to those following ingestion, although blood disorders are less prominent. Headache, weakness, eye irritation, cyanosis, nausea, and vomiting appear first, followed by loss of consciousness and respiratory and circulatory failure. Postmortem findings often include damage to the liver, kidneys, and lungs.

Chronic Toxicity:

In tests by the National Cancer Institute ethylene dichloride has been shown to be carcinogenic in both rats and mice and therefore should be considered as a suspected human carcinogen.

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Sampling and Analytical Methods

- 1. NIOSH Method 1003
 - a. Charcoal absorption.
 - b. Carbon disulfide desorption.
 - c. Gas chromatography.
 - d. Flame ionization detector.

Detection limit:

- 0.7 ppm for ethylene dichloride per 3-liter sample
- 0.6 ppm for p-dichlorobenzene per 3-liter sample

Possible interferences: None identified.

- 2. Method B (Appendix A): C_2-C_{18} hydrocarbons and other nonpolar organics with a boiling point of 100° to 175°C.
 - a. Whole air collection in canister.
 - b. Cryogenic concentration.
 - c. Gas chromatography/flame ionization detection (gas chromatography/electron capture detection may also be used).

Detection limit: 0.1 ppb per 100-ml sample

Possible interferences: Storage times greater than a week are not recommended.

- 3. Method C (Appendix A): C_6-C_{12} hydrocarbons and other nonpolar organics with boiling point between 60° and 200°C. a. Adsorption on Tenax.
 - b. Thermal desorption.
 - Gas chromatography/mass spectrometry analysis (gas chromatography/electron capture detection also may be used).

Detection limit: 1 to 200 ppt per 20-liter sample

Possible interferences:

Blank levels usually limit sensitivity; artifacts due to reactive components $(0_3, NO_x)$ can be a problem. Sample can be analyzed only once.

- 4. Method D (Appendix A): C_6-C_{12} hydrocarbons and other nonpolar organics with boiling point of 60° to 200°C.
 - a. Adsorption on Tenax.

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- b. Thermal desorption into canisters.
- c. Gas chromatography/flame ionization detection, or gas chromatography/mass spectrometry analysis (gas chromatography/electron capture detection also may be used.)

	Solid waste	Water
Emission factor, kg/mt		
Direct chlorination Oxychlorination	1.5 2.8	2.9 4.6
Emissions, ^a 1000 mt/yr		
Direct chlorination Oxychlorination	4.5 6.1	8.5 10.0
Total emissions	10.6	18.5

TABLE E-30. ESTIMATED 1977 EDC EMISSIONS AS SOLID WASTE AND TO WATER FROM ETHYLENE DICHLORIDE PRODUCTION

^aAssumes 58 percent direct chlorination and 42 percent oxychlorination and an EDC production of 5,194,000 mt/yr.

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Source: SRI International, 1979.

- International Agency for Research on Cancer. 1979. <u>IARC Monographs on the</u> <u>Evaluation of Carcinogenic Risk of Chemicals to Man</u>. <u>Volume 20</u>, <u>1,2-Dichloroethane</u>. Lyon, France. pp. 429-448.
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Chemical Name

Ethylene dibromide

CAS Number

106-93-4

Chemical Classification

Halogenated hydrocarbon (unsaturated)

Synonyms

Aethylenbromid; bromofume; bromuro di etile; celmide; DBE; 1,2dibromaethan; 1,2-dibromoethano; dibromoethane; alpha-beta-dibromoethane; sym-dibromoethane; 1,2-dibromoethane; 1,2-dibromoethane (DOT); dibromure d'ethylene; 1,2-dibromethaan; dow fume 40; dowfume EBD; dowfume W-8; dowfume W-85; dwubrometan; EDB; EDB-85; E-D-Bee; ENT 15,349; ethylene bromide; ethylene dibromide; ethylene dibromide (DOT); 1,2-ethylene dibromide; fumo-gas; glycol bromide; glycol dibromide; iscobrome-D; kopfume; NCI-C00522; nephis; pestmaster; pestmaster EDB-85; soilbrom-40; soilbrom-85; soilbrome-85; soilbrom-90EC; soilfume; unifume.

Physical/Chemical Properties

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Description:
     Colorless, nonflammable liquid, sweet odor, emulsifiable.
Boiling Point:
     131°C
Melting Point:
     9°C
Molecular Weight:
      187.9
Chemical Formula:
     BrCH<sub>2</sub>CH<sub>2</sub>Br
Vapor Pressure:
     17.4 mm at 30°C
Vapor Density:
     6.48 (air = 1)
Refractive Index:
     N_{D}^{20} = 1.5387
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Solubility:

Miscible with most solvents and thinners; slightly soluble in water.

Log Partition Coefficient (octanol/water): Not available

Photochemical Reactivity:

Ethylene dibromide resists atmospheric oxidation by peroxides and ozone, typically showing half-lives in excess of 100 days in those reactions. Generally less reactive in the atmosphere than corresponding alkanes or olefins.

Chemical Reactivity:

Reacts as alkylating agent and liberates bromide. The chemical has a half-life of 5 to 10 days toward hydrolysis under neutral conditions at ambient temperature in an aquatic environment. Generally inert at normal temperatures, although slight decomposition may result from exposure to light. It is hydrolized to ethylene glycol and bromothanol at elevated temperatures. When heated to 340° to 370°C, ethylene dibrodmide decomposes to vinyl bromide and hydrobromic acid. The terminal halogen atoms are reactive, which makes the compound a useful synthetic intermediate. It is the least expensive organic bromine compound available.

Environmental Fate

C-Br bond can photolyze in atmosphere. Photooxidation is probably important in the atmosphere. Volatilization is the major transport mechanism. It is not known whether rates of atmospheric degradation are sufficient to handle the environmental burden adequately. In about 2 months, EDB is converted almost completely and quantitatively to ethylene in soil culture.

Source of Emissions

Production:

Action of bromine on ethylene.

Uses:

Scavenger for lead in gasoline (over 85 percent, used for this purpose. This use will be phased out as leaded gasoline is phased out.) Grain fumigant General solvent Waterproofing preparations Organic synthesis, including vinyl bromide Fumigant for tree crops Tables E-31 through E-35 present ethylene dibromide

production, consumption, and emission data.

Location	EDB capacity, 10 ⁶ kg	Production of vinyl bromide	Production of fumigant	TEL ^a capacity, 10 ⁶ kg	Estimated EDB ^D use for TEL, 10 ⁶ kg
Arkansas					
El Dorado Great Lakes Chemical Corp	23		v		
Magnolia	23		^		
Dow Chemical Co	14		x		
Ethyl Corp. (Bromet Co.)	$\frac{68}{99}$				
lotal	82	×	X		
California]				
Antioch				70	
E. I. Du Pont de Nemours & Co., Inc.				/9	14
Louisiana	ł	{			
Baton Rouge					
Ethyl Corporation				79	14
Michigan					
Midland	ł				
Dow Chemical Company	39	×	x		
New Jersev					
Deepwater					
E. I. Du Pont de Nemours & Co., Inc.]			79	14
Teras					
Beaumont					
Houston Chemical Company					
(PPG Industries)	16		x	54	10
Nalco Chemical Company				18	3
Pasadena	4				ľ
Ethyl Corporation				79	14

TABLE E-31. CAPACITIES OF ETHYLENE DIBROMIDE MANUFACTURING AND FORMULATING FACILITIES

Source: SRI International, 1978.

^aTetraethyl lead.

^bEthylene dibromide.

.

		Amon	Automobile	Emission rate,	Wind	EDB ^b concentration		
SMSA	Population	10 ⁹ m ²	registration	g/s-m ²	speea m/s	10 ⁻³ µg/m ³	ppt	
SMSAs >2,000,000								
Pittsburgh San Francisco	2,333,600 3,135,900	7.8 6.2	2,358,600 688,300	4.8 1.8	5 3	2.1 1.4	0.3 0.2	
SMSAs 1,000,000 - 2,000,000								
Columbus, OH Milwaukee	1,055,900 1,423,000	6.2 3.7	567,803 642,531	1.7 2.8	5 5	0.66 1.2	0.90 0.2	
SMSAs 500,000 - 1,000,000								
Sacramento Providence - Warwick	851,300	8.7	439,803	0.80	3	0.60	0.08	
Pawtucket	854,400	2.4	869,100	5.8	7	1.9	0.2	
SMSAs 250,000 - 500,000								
Wichita Harrisburg	375,600 425,500	6.2 4.1	221,715 198,997	0.57 0.77	7 5	0.18 0.35	0.02 0.05	

TABLE E-32. ESTIMATES OF ANNUAL AVERAGE ETHYLENE DIBROMIDE CONCENTRATIONS FOR SELECTED SMSAs

^aAssumes 80 percent of vehicles use leaded gasoline.

^bEthylene dibromide.

Source: SRI International, 1978.

							EC	B ^b cond	ncentration		
	AZMZ	City	City		Emission rate a Wind	Wind	Central	city	Subu	ırban	
City	population, 10 ³	population, 10 ³	area, 10 ⁹ m²	Automobile registration	10 ⁻¹⁰ g/s-m ²	speed, m/s	10 ⁻ з µg/m ³	ppt	10 ⁻ 3 µg/m ³	ppt	
Chicago	6,998.8	3,173	0.57	1,324,171	3.71	5	16	2.1	6.6	0.9	
Detroit	4,446.3	1,387	0.35	675,065	3.08	6	11	1.4	7.7	1.0	
Houston	2,163.4	1,320	1.1	701,766	1.01	6	4	0.5	0.74	0.1	
Los Angeles	6,938.3	2,747	1.2	1,490,483	1.98	3	14	1.8	3.0	0.4	
New York	9,746.4	7,647	0.77	1,707,891	3.54	7	11	1.4	1.8	0.2	
Philadelphia	4,826.3	1,862	0.33	944,660	4.57	6	17	2.2	1.0	0.1	

TABLE E-33. ESTIMATES OF AVERAGE ANNUAL ETHYLENE DIBROMIDE CONCENTRATIONS FOR CITIES WITH POPULATIONS EXCEEDING 1,000,000

^aAssumes 80 percent of vehicles use leaded gasoline.

^bEthylene dibromide.

Source: SRI International, 1978.

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Company	Location	Number of sites ^a	Total sampling time, h	Concen- tration,c ppb	Standard deviation
Dow	Magnolia, Ark.	1	4	13.2	0.9
Ethyl Corp.	Magnolia, Ark.	1	8	3.1	4.3

TABLE E-34. RESULTS OF ETHYLENE DIBROMIDE MONITORING IN THE VICINITY OF MANUFACTURING FACILITIES

^aAll sites were within 100 m of the plant.

^bSamples were discontinuous; two were taken near the Dow facility and five near the Ethyl Corporation facility.

^CTo convert to μ g/m³, divide by 0.13.

Source: SRI International, 1978.

			Estim EDB	ated level	
Customer	Nozzle time, min	gallons pumped	µg/m³	ppt	
1	2.5	14	0.345	45	
2	1.1	8	0.972	126	
3	1.6	9	5.220	679	

TABLE E-35. ESTIMATES OF ETHYLENE DIBROMIDE EXPOSURES FROM SELF-SERVICE GASOLINE PUMPS

Average Nozzle Time = 1.7 min.

Time-weighted average exposure = 260 ppt.

^aEthylene dibromide.

Source: SRI International, 1978. The conversion is based on differences in vapor pressure and concentration between benzene and ethylene dibromide in gasoline.
Storage and Transportation:

Protection against physical damage is required. Should be stored in cool, dry, well-ventilated location, away from any area where the fire hazard may be acute. Shipped in glass bottles, metal drums, and tank cars.

Disposition:

Ethylene dibromide may be disposed of by controlled incineration with adequate scrubbing and ash disposal facilities.

Sampling and Analytical Methods

- NIOSH Method 1008

 a. Solid Sorbent Tube (coconut shell charcoal, 100 mg/50 mg).
 - b. Gas chromatography, electron capture detector.

Detection limit: 0.04 mg/m³ per 25-liter sample

Possible interferences: None idnetified.

2. NIOSH Method S104

- a. Adsorption with charcoal.
- b. Desorption with carbon disulfide.
- c. Gas chromatography.

Detection limit: 22 to 660 mg/m³ per 1-liter sample

Possible interferences: Any compound that has the same retention time may interfere. High humidity.

Permissible Exposure Limits

	OSHA	ACGIH	NIOSH
TWA Ceiling Peak	20 ppm 30 ppm 50 ppm (5 min)	none	1 mg/m ³ (15 min)

The ACGIH lists ethylene dibromide as an industrial substance suspected of carcinogenic potential for man (skin).

Human Toxicity

Acute Toxicity:

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Severe skin irritant. Serious toxic interaction between inhaled ethylene dibromide and ingested disulfiram. One case of fatal poisoning reported after ingestion of 4.5 ml. Patient vomited recurrently, had watery diarrahea, became anuric, and died 2 days later. Massive damage of the kidneys noted at autopsy.

Chronic Toxicity:

Both the National Cancer Institute and the National Toxicology Program have found ethylene dibromide to be carcinogenic in both mice and rats; therefore, it can be considered a suspected human carcinogen.

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Chemical Name

Ethylene oxide

CAS Number

65-21-8

Chemical Classification

Epoxide

Synonyms

Aethylenoxid; anprolene; benvicide; carboxide; cry-oxide; dihydroxirene; dimethylene oxide; E.O.; 1,2-epoxyacthan; epoxyethane; 1,2-epoxyethane; ethyleen oxide; ethylene oxide (DOT); ethylene (oxide'd); etilene (ossido di); ETO; eto; etylenutlener; NCI-C50088; oxacyclopropane; oxane; oxidoethane; alpha-beta-oxidoethane; oxiraan; oxiran; oxirane; oxirene, dihydro-; oxyfume 12; oxyfume sterilant 20; pennoxide, steroxide 12; steroxide 20; t-gas;

Physical/Chemical Properties

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Desci	ription: Colorless ppm.	gas at	: room	tempera	ature. E	Ether-li	ke odo	r over	700
Boil	ing Point: 10.73°C								
Melt	ing Point: -111.3°C								
Mole	cular Weig 44.1	ht:							
Chem	ical Formu CH ₂ CH ₂ O	la:							
Vapo	r Pressure 1095 mm a	: t 20°C							
Vapo	r Density: 1.52 (air	= 1)							
Refr	active Ind N _D ⁷ = 1.3	ex: 597							
Solui	bility: Soluble i portions.	n orgaı	nic so	lvents;	miscible	e with w	vater i	n all	pro-

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Log Partition Coefficient (octanol/water): -0.3

Photochemical Reactivity: Reactivity toward OH• is the same as butane. No reaction toward photolysis.

Chemical Reactivity:

Reacts readily with proton donors such as alcohols, amines and thiols. Decomposes violently at temperatures above 800°C. Ethylene oxide will polymerize violently if contaminated with aqueous alkalies, amines, mineral acids, metal chlorides, or metal oxides. Incompatible with alkalines and acids. Reacts with active hydrogen compounds (e.g., alcohols, amines, and sulphydryl compounds) and with inorganic chloride in food to form ethylene chlorohydrin. Also reacts with 4-4'-nitrobenzyl pyridine.

Environmental Fate

In connection with the treatment of foods with ethylene oxide, the compound reacts with inorganic chloride to form ethylene chlorohydrin.

Source of Emissions

Production:

From oxidation of ethylene in air or oxygen with silver catalyst.

From the reaction of ethylene with hypochlorous acid followed by dehydrochlorination of the resulting chlorohydrin with lime (chlorohydrin process).

Uses:

Manufacture of ethylene glycol and higher glycols Surfactants Acrylonitrile Ethanolamines Petroleum demulsifier Fumigant Rocket propellant Industrial sterilant, e.g., medical plastic tubing Fungicide

Tables E-36 through E-41 and Figure E-2 present data on ethylene oxide production, consumption, and emissions.

Storage:

Should be protected against physical damage. Should be kept cool, below 86°F. Should be stored outside, away from buildings and other materials, in insulated tanks or containers, shielded from sun and heat or provided with cooling facilities and protected by a properly designed water-spray system.

Source	Location	Type of process ^a	1978 estimated production, ^b 10 ⁶ lb/yr	1978 estimated capacity, 10 ⁶ 1b/yr	Geographic coordinates
BASF Wayandotte	Geismar, LA	В	222	310	30 11 34/91 00 42
Celanese	Clear Lake, TX	В	340	475	29 37 17/95 03 51
Dow .	Freeport, TX Plaquemine, LA	A A	322 351	450 490	28 59 15/95 24 45 30 19 00/91 15 32
Jefferson Chemical	Port Neches, TX	Α	340	475	29 57 45/93 56 00
Northern Petrochemical	East Morris, IL	В	165	230	41 24 08/88 17 18
01in	Brandenburg, KY	В	75	105	38 00 27/86 06 50
PPG	Beaumont, TX	ß	107	150	30 03 40/94 02 30
Shell Chemical	Geismar, LA	В	193	270	30 11 00/90 59 00
Sunolin Chemical	Claymont, DE	В	72	100	39 48 20/75 25 40
Texas Eastman	Longview, TX	В	136	190	32 25 55/94 41 06
Union Carbide	Seadrift, TX Taft, LA	A A	594 723	830 1010	28 30 31/96 46 18 29 58 00/97 27 00
Total	ال مع رية من معالم معا	L	3640	5085	

TABLE E-36. ETHYLENE OXIDE PRODUCERS

^aA = air oxidation process. B = oxygen oxidation process.

^bThe distribution of production for each producer is determined by the ratio of total U.S. production/ total capacity times individual site capacity.

Source: Systems Applications, Inc. 1980.

		1978 capacity (1b x 10 ⁶)					
Source	Location	Ethylene oxide	Ethylene glycol	Diethylene glycol	Triethylene glycol	Glycol ethers	Ethanol- amines
BASF Wayandotte	Geismar, LA	310		20		230	
Celanese	Clear Lake, TX	475		50	10		
Dow .	Freeport, TX Plaquemine, LA	450 490	330 550	25 50	50		40 100
Jefferson	Port Neches, TX	475	360	35	20	40	80
Northern Petrochemical	East Morris, IL	230	350	35			
Olin	Brandenburg, KY	105	50	5	2	70	25
PPG	Beaumont, TX	150	200	20		20	
Shell Chemical	Geismar, LA	270	200	20	5	50	
Sunolin Chemical	Claymont, DE	100					ļ
Texas Eastman	Longview, TX	190	180	20		25	
Union Carbide	Seadrift, TX Taft, LA	830 1010	870 1200	80 100	75 ^a	490 ^a	230
ICI Americas	Hopewell, VA		33				

TABLE E-37. ETHYLENE OXIDE PRODUCERS AND USERS

^aIncludes a plant in Penuelas, Puerto Rico.

Source: Systems Applications, Inc. 1982.

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	Usa	age
	10 ⁶ 1b/yr	%
Ethylene glycol polyester	910	25
Ethylene glycol antifreeze	837	23
Ethylene glycol (other uses)	364	10
Surface active agents	546	15
Ethanolamines	255	7
Glycol ethers	255	7
Other	473	13
Total	3640	100

TABLE E-38. END-USE DISTRIBUTION OF ETHYLENE OXIDE IN 1978

Source: Systems Applications, Inc., 1980.

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	Production/		Total emissions		
Source	usage 10 ⁶ lb/yr	Usage %	lb/yr	g/s	
Producers ^a					
Air oxidation	2330		1,277,000	18.4	
Oxygen oxidation	1310		410,900	5.9	
Users					
EG ^b polyester	910	25			
EG antifreeze	837	23			
EG (other uses)	364	10			
Surface active agents	546	15			
Ethanolamines	255	7			
Glycol ethers	255	7			
Other	473	13			
Total			1,687,900	24.3	

TABLE E-39. ESTIMATED 1978 NATIONWIDE EMISSIONS OF ETHYLENE OXIDE

^aTotal emissions from producers also include total emissions from users since ethylene oxide is produced and used at the same site. ^bEG = ethylene glycol.

Source: Systems Applications, Inc., 1982.

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		Process	Storage	Fugitive	Total emissions	
Company	Location	emissions, lb	emissions, lb	emissions,	16	g/s
Dow	Freeport, TX Plaguemine, LA	169,000 184,000	6,880 7,500	529 577	176,000 192,000	2.5 2.8
Jefferson	Port Neches, TX	179,000	7,270	559	187,000	2.7
Union Carbide	Seadrift, TX Taft, LA	312,000 380,000	12,700 15,500	977 1,190	326,000 397,000	4.7 5.7
Total		1,224,000	49,850	3,832	1,278,000	18.4

TABLE E-40. ETHYLENE OXIDE EMISSIONS FROM PRODUCERS (Air Oxidation Process)

Source: Systems Applications, Inc. 1982.

		Process	Storage	Fugitive	Total emissions	
Company	Location	lb	emissions, lb	lb	۱b	g/s
BASF	Geismar, LA	1,032	156	12	1,200	.02
Celanese	Clear Lake, TX	135	12	1,853	2,000	.03
Northern Petrochemical	Port Neches, TX	77,340	11,690	899	89,930	1.3
Olin	Brandenburg, KY	35,150	5,314	409	40,880	0.6
PPG	Beaumont, TX	50,150	7,581	583	58,320	0.8
Shell Chemical	Geismar, LA	90,460	13,670	1,052	105,200	1.5
Sunolin Chemical	Claymont, DE	33,750	5,101	392	39,240	0.6
Texas Eastman	Longview, TX	63,740	9,636	741	74,120	1.1
Total		351,667	53,158	5,942	410,900	5.9

TABLE E-41. ETHYLENE OXIDE EMISSIONS FROM PRODUCERS (Oxygen Oxidation Process)

Source: Systems Applications, Inc. 1982.



NOTE: NUMERALS DENOTE NUMBER OF PLANTS.

Figure E-2. Specific point sources of ethylene oxide emissions Source: Systems Applications, Inc. 1980.

Adequate diking and drainage should be provided in tank area to confine and dispose of liquid in case of a tank rupture. Pits and depressions should be avoided. Inside storage should be held at a minimum and confined to a standard fire-resistant flammable liquids storage room, provided with continuous ventilation and free of sources of ignition.

Transportation:

Shipped in steel cylinders, drums, insulated tank cars, and tank barges. The U.S. Bureau of Explosives requires a red label on all shipments. Not acceptable on passenger planes.

Disposition:

Ethylene oxide may be disposed of as a concentrated waste containing no peroxide by discharging liquid at a controlled rate near a pilot flame or as a concentrated waste containing peroxides by perforation of a container of the waste from a safe distance followed by open burning. Ethylene oxide is a hazardous waste with a hazardous waste number of U 115 assigned by EPA.

Sampling and Analytical Methods

- 1. NIOSH Method S286
 - a. Adsorption on charcoal.
 - b. Desorption with carbon disulfide.
 - c. Gas chromatography.

Detection limit:

20 to 270 mg/m³ for a 5-liter sample.

Possible interferences:

High humidity. Any compound with the same retention time may cause an interference.

- 2. Method A (Appendix A)
 - a. Direct gas injection into gas chromatograph/flame.
 - b. Ionization detector.

Detection limit: 0.01 ppm

Possible interferences: Losses from surface adsorption may occur in some cases.

- 3. Method B (Appendix A) C_2-C_{18} hydrocarbons and other nonpolar organics with a boiling point of 100° to 175°C
 - a. Whole air collection in canister.
 - b. Cryogenic concentration.
 - c. Gas chromatography/flame ionization detection.

Detection limit: 0.1 ppb per 100-ml sample

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Possible interferences:

Water soluble compounds are not readily analyzed. Storage times greater than a week are not recommended.

- 4. Method E (Appendix A)
 - a. Adsorption on charcoal.
 - b. Desorption with CS₂.
 - c. Analysis by gas chromatography/flame ionization detection.

Detection limit:

0.1 to 1 ppm per 10-liter sample

Possible interferences: Sensitivity much poorer than for thermal desorption.

Permissible Exposure Limits

 OSHA
 ACGIH

 TWA
 1 ppm
 1 ppm (2 mg/m³)

The ACGIH lists ethylene oxide as an industrial substance suspected of carcinogenic potential for man.

Human Toxicity

Acute Toxicity:

Powerful irritant (systemic). High toxicity effect through oral, inhalation, intraperitoneal, and intravenous means. An irritant to skin, eyes, and mucous membranes of respiratory tract. High concentrations can cause pulmonary edema.

Chronic Toxicity:

Tests on rats found ethylene oxide to be an equivocal tumorigenic agent. Currently tested by the National Toxicology Program for carcinogenesis bioassay.

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Chemical Name

Formaldehyde

CAS Number

50-00-0

Chemical Classification

Aldehyde

Synonyms

Aldehyde formique; aldehyde formica; BFV; FA; fannoform; formaldehyd; formaldehyde, as formalin solution (DOT); formalin-loesungen; formalith; formicaldehyde; formel; FYDE; hoch; ivalon; karsan; cysoform; methanal; methylaldehyde; methylene glycol; methylene oxide; morbicide; NCI-C02799; opplossingen; oxomethane; oxymethylene; paraform; polyoxymethylene glycols; superlysoform; tetraoxynethylene; trioxane

Physical/Chemical Properties

Description: Gas; strong pungent odor. Boiling Point: -19°C Melting Point: -118°C Molecular Weight: 30.0 Chemical Formula: нсно Vapor Pressure: 760 mm at -19.5°C Vapor Density: 1.067 (air = 1) **Refractive Index:** Not available Solubility: Soluble in water and alcohol.

Log Partition Coefficient (octanol/water): -0.96

Photochemical Reactivity:

Reactivity toward OH• is 2 to 4 times butane. Photolysis is 9 percent per hour at full sunlight. Major atmospheric precursors are hydrocarbons (photooxidation). Formed by incomplete combustion of many organic substances. Equilibrium is approximately 5 percent for methane hydrocarbons.

Chemical Reactivity:

Reacts with NO at about 180° F, when the reaction becomes explosive. Also reacts violently with $H10_4$ -aniline and performic acid, nitromethane, magnesium carbonate, and hydrogen peroxide. Can react with hydrogen chloride and inorganic chlorides to yield bis-chloromethyl ether (BCME) which is a potent carcinogen. This reaction occurs only at high (500 to 3,000 ppm) concentrations.

Environmental Fate

Bioaccumulation of formaldehyde is unlikely due to its high chemical reactivity. Degradation in the atmosphere is by photochemical process, and it biodegrades to formic acid, methyl alcohol, carbon dioxide, and water.

Source of Emissions

Production:

Oxidation of synthetic methanol or low boiling petroleum gases such as propane and butane. The most common catalysts are silver, copper, or iron-molybdenum.

Uses:

Urea and melamine resins
Polyacetal resins
Phenolic resins
Ethylene glycol
Pentaerythritol
Hexamethylenetetramine
Fertilizer
Dyes, medicine (disinfectant, germicide)
Embalming fluids
Preservative
Hardening agent
Reducing agent, as in recovery of gold and silver
Corrosion inhibitor in oil wells
Durable-press treatment of textile
Industrial sterilant
Treatment grain

Tables E-42 through 4-46 and Figure E-3 present formaldehyde production, consumption and emission data.

Source	Location	1978 Estimated production, _a 10 ⁶ lb/yr	1978 Estimated capacity, 10 ⁶ 1b/yr	Geographic coordinates, Latitude/longitude
Allied Chemical	South Point, OH	222	310	38 25 43/82 36 00
Borden, Inc.	Demopolis, AL Diboll, TX Fayetteville, NC Geismar, LA Louisville, KY Sheboygan, WI Fremont, CA Kent, WA LaGrande, OK Missoula, MT Springfield, OR	72 57 168 179 57 93 161 57 46 64 172	100 80 235 250 80 130 225 80 65 90 240	$\begin{array}{cccccccccccccccccccccccccccccccccccc$
Celanese Chemical	Bishop, TX Newark, NJ Rock Hill, SC	1075 84 84	1500 117 117	27 34 06/97 49 27 40 43 30/74 07 25 34 57 25/80 57 32
Chembond Corp.	Springfield, OR Winnifield, LA	107 50	150 70	44 02 60/122 59 06 31 54 49/92 40 35
Du Pont	Belle, WV LaPorte, TX Healing Springs, NC Linden, NJ Toledo, OH	358 229 158 115 193	500 320 220 160 270	38 12 13/81 28 34 29 42 04/95 02 05 35 01 56/80 10 30 40 36 02/74 12 08 41 39 22/83 33 20
GAF Corp.	Calvert City, KY	72	100	37 02 50/88 21 12

TABLE E-42. PRODUCTION OF FORMALDEHYDE

(continued)

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TABLE E-42 (continued)

Source	Location	1978 Estimated production, 10 ⁶ lb/yr ^a	1978 Estimated capacity, 10 ⁶ lb/yr	Geographic coordinates, Latitude/longitude
Georgia-Pacific Corp.	Albany, OR Columbus, OH Coosbay, OR Crossett, AR Russelville, SC Taylorsville, MS Vienna, GA Lufkin, TX	86 72 65 115 143 86 72 72	120 100 90 160 200 120 100 100	44 37 07/123 05 13 39 53 07/82 56 45 42 27 26/124 10 47 33 08 36/93 02 11 33 20 52/79 58 00 39 51 00/89 25 00 37 07 30/83 49 00 31 21 00/94 47 00
Gulf Oil Corp.	Vicksburg, MS	43	60	32 17 00/90 54 00
Hercules Inc.	Louisiana, MO Wilmington, NC	122 72	170 100	39 26 24/91 03 37 34 19 09/77 59 23
Hooker Chemicals & Plastics	Tonawanda, NY	97	135	43 02 47/78 51 44
IMC Chemical Group	Seiple, PA Sterlington, LA	47 22	65 30	40 38 12/75 31 58 32 43 25/92 08 56
Monsanto Corp.	Addyston, OH Chocolate Bayou, TX Eugene, OR Springfield, MA	72 140 72 211	100 195 100 295	39 07 30/84 42 58 29 14 55/95 12 45 44 02 59/123 08 19 42 09 33/72 29 09
Pacific Resins and Chemicals	Eugene, OR	68	95	44 01 00/123 05 05
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TABLE E-42 (continued)

Source	Location	1978 Estimated production, 10 ⁶ lb/yr ^a	1978 Estimated capacity, 10 ⁶ lb/yr	Geographic coordinates, Latitude/longitude
Reichhold Chemicals, Inc.	Hampton, SC	36	50	32 53 33/81 06 10
	Houston, TX	86	120	29 44 50/95 10 00
	Kansas City, KA	36	50	39 09 28/94 37 41
	Malvern, AR	79	110	34 24 09/92 48 45
	Moncure, NC	86	120	35 31 18/79 04 52
	Tacoma, WA	36	50	47 16 11/122 22 57
	Tuscaloosa, AL	50	70	33 12 03/87 34 00
	White City, OR	179	250	42 26 18/122 07 07
Tenneco, Inc	Fords, NJ	133	185	40 30 50/74 19 17
	Garfield, NJ	72	100	40 52 28/74 06 49
Wright Chemical Corp.	Riegelwood, NC	57 6,400	80 8,929	34 19 22/78 12 09

^aThe distribution of production for each producer is determied by the ratio of total U.S. production to total U.S. capacity as compared to individual plant opacity.

Source: System Applications, Inc. 1982.

End-Use	Percent of total consumption	End-use consumption 10 ⁶ lb/yr
Urea resins	25.4	1630
Phenolic resins	24.3	1560
Butanediol	7.7	490
Acetal resins	7.0	450
Pentaerythritol	6.0	380
Hexamethylenetetramine	4.5	290
Melamine resins	4.2	270
Urea formaldehyde concentrates	3.6	230
Chelating agents	3.6	230
Trimethylolpropane	1.3	80
Other Chemical intermediate uses	11.9	760
Export	0.5	30
Total	100.0	6400

TABLE E-43. FORMALDEHYDE CONSUMPTION BY END USE

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TABLE E-44. FORMALDEHYDE CHEMICAL INTERMEDIATE USERS

Source	Location	1978 Estimated formaldehyde consumption, 10 ⁶ 1b	Geographic coordinates, Latitude/longitude
Butanediol ProductionDu Pont CompanyHouston, TXGAF CorporationCalvert City, KYTexas Citv. TX		240 80 80	29 42 04/95 02 05 37 02 50/88 21 12 29 25 29/94 58 07
Total		400	
Acetal Resins Production Celanese Corporation Du Pont Company Total	Bishop, TX Parkersburg, WV	310 140 450	27 34 06/97 49 27 39 15 27/81 32 52
Pentacrythritol Production Celanese Corporation Hercules, Inc. IMC (CSC) Perstop AB Total	Bishop, TX Louisiana, MO Seiple, PA Toledo, OH	160 100 50 70 380	27 34 06/97 49 27 39 26 24/91 03 37 40 38 12/75 31 58 41 42 33/83 30 00
Hexamethylenetetramine Production Borden, Inc. W. R. Grace & Company Occidental Petroleum Co. Plastics Engineering Co. Tenneco, Inc. Wright Chemical Corp. Total	Fayetteville, NC Nashua, NH North Tonawanda, NY Sheboygan, WI Fords, NJ Acme, NC	60 60 50 20 40 60 290	35 01 43/78 51 41 42 46 00/71 27 52 43 02 47/78 51 44 43 45 00/87 47 00 40 30 50/74 19 17 34 19 22/78 12 09
Trimethylolpropane Production Celanese Corp.	Bishop, TX	80	27 34 06/97 49 27

Source: System Applications, Inc. 1982.

		1978	Tunn of	Process	Storage	Fugitive	Total em	issions
Company	Location	10 ⁶ 1b	process	104 1b	104 1b	104 1b	104 16	g/s
Allied Chemical	South Point, OH	222	A	5.81	0.46	0.91	7.19	1.04
Borden, Inc.	Demopolis, AL Diboll, TX Fayetteville, NC Geismar, LA Louisville, KY Sheboygan, WI Fremont, CA	72 57 168 179 57 93 161	A A A A A A	1.89 1.49 4.40 4.69 1.49 2.44 4.22	0.15 0.12 0.35 0.37 0.12 0.19 0.33	0.30 0.23 0.69 0.74 0.23 0.38 0.66	2.33 1.85 5.44 5.79 1.85 3.01 5.21	0.34 0.27 0.78 0.83 0.27 0.43 0.75
	Kent, WA LeGrande, OR Missoula, MT Springfield, OR	57 46 64 172	A A A	1.49 1.21 1.68 4.51	0.12 0.09 0.13 0.35	0.23 0.19 0.26 0.71	1.85 1.49 2.07 5.57	0.27 0.21 0.30 0.80
Celanese Chemical	Bishop, TX Newark, NJ Rock Hill, SC	1075 84 84	A B B	8.84 3.30 3.30	0.70 0.43 0.43	1.36 0.68 0.68	10.98 4.41 4.41	1.58 0.63 0.63
Chembond Corp.	Springfield, OR Winnifield, LA	107 50	B B	4.20 1.96	0.55 0.26	0.86 0.40	5.62 2.62	0.81 0.38
Du Pont	Belle, WV LaPorte, TX Healing Springs, NC Linden, NJ Toledo, OH	358 229 158 115 193	A A A A	9.38 6.00 4.14 3.01 5.06	0.74 0.47 0.33 0.24 0.40	1.47 0.94 0.65 0.47 0.79	11.59 7.41 5.11 3.72 6.25	1.67 1.07 0.74 0.54 0.90
GAF Corp.	Calvert City, KY	72	B	2.83	0.37	0.58	3,78	0.54
Georgia-Pacific Corp.	Albany, OR Columbus, OH Coos Bay, OR Crossett, AR Russelville, SC Taylorsville, MS Vienna, GA Lufkin, TX	86 72 65 72 43 143 86 72 72	B B A B B A B	3.38 2.83 2.55 0.00 5.61 3.38 0.00 0.00	0.44 0.37 0.34 0.15 0.22 0.74 0.44 0.15 0.37	0.69 0.58 0.30 0.35 1.15 0.69 0.30 0.58	4.51 3.78 3.41 0.45 0.57 7.51 4.51 0.45 0.95	0.65 0.54 0.06 0.08 0.33 1.08 0.65 0.06 0.14
Gulf Oil Corp.	Vicksburg, MS	43	8	1.69	0.22	0.35	2.26	0.33
Hercules Inc.	Louisiana, MO Wilmington, NC	122 72	A A	3.20 1.89	0.25 0.15	0.50 0.30	3.95 2.33	0.57 0.34
Hooker Chemicals & Plastics	Tonawanda, NY	97	A	2.54	0.20	0.40	3.14	0.45
IMC Chemical Group	Seiple, PA Sterlington, LA	47 22	A A	1.23 0.58	0.10 0.05	0.19 0.09	1.52 0.71	0.22 0.10

TABLE E-45. 1978 FORMALDEHYDE PRODUCTION EMISSIONS

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TABLE	E-45	(continued)

		1978	Turne	Process	Storage	Fugitive	Total em	issions
Company	Location	10 ⁶ 1b	process	104 lb	104 1b	emissions, 104 1b	104 16	g/s
Monsanto Corp.	Addyston, OH Chocolate Bayou, TX Eugene, OR Springfield, MA	72 140 72 211	A A A	0.34 0.66 0.34 1.00	0.03 0.05 0.03 0.08	0.05 0.11 0.05 0.16	0.42 0.82 0.42 1.23	0.06 0.12 0.06 0.18
Pacific Resins and Chemicals	Eugene, OR	68	A	1.78	0.14	0.28	2.20	0.32
Reichhold Chemicals, Inc.	Hampton, SC Houston, TX Kansas City, KA Malvern, AR Moncure, NC Tacoma, WA Tuscaloose, AL White City, DR	36 86 79 86 36 50 179	A B B B B B B	0.94 3.38 0.94 3.10 3.38 1.41 1.31 7.03	0.07 0.44 0.07 0.41 0.44 0.19 0.10 0.93	0.15 0.69 0.15 0.64 0.69 0.29 0.21 1.44	1.17 4.51 1.17 4.15 4.51 1.89 1.62 9.40	0.17 0.65 0.17 0.60 0.65 0.27 0.23 1.35
Tenneco, Inc	Fords, NJ Garfield, NJ	71 62 72	A B A	1.86 2.43 1.89	0.15 0.32 0.15	0.29 0.50 0.30	2.30 3.25 2.33	0.33 0.45 0.34
Wright Chemical Corp.	Riegelwood, NC	57	В	2.24	0.29	0.46	2.99	0.43
Total		6400		150.24	15.76	30.86	193.97	27.92

Source: Systems Applications, Inc., 1982.

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		Process	Storage	Fugitive	Total emissions	
Source	Location	lb/yr	lb/yr	1b/yr	lb/yr	g/s
Butanediol Producers						
Du Pont Company	Houston, TX	480,000	120,000	120,000	720.000	10.37
GAF Corporation	Calvert City, KY	160,000	40,000	40,000	240,000	3.46
	Texas City, TX	160,000	40,000	40,000	240,000	3.46
Total		800,000	200,000	200,000	1,200,000	
Acetal Resins Producers						······································
Celanese Corporation	Bishop, TX	391,409	48,927	48,927	489.263	7.04
Du Pont Company	Parkersburg, WV	560,000	70,000	70,000	700,000	10.08
Total		951,409	118,927	118,927	1,189,263	· · · · · · · · · · · · · · · · · · ·
Pentacrythritol Producers						
Celanese Corporation	Bishop, TX	369,208	44,445	20,708	434.361	6.25
Hercules, Incorporated	Louisiana, MO	731,000	88,000	41,000	860.000	12.38
IMC (CSC)	Seiple, PÁ	365,500	44,000	20,500	430,000	6.19
Perstorp AB	Toledo, OH	511,700	61,600	28,700	602,000	8.67
Total		1,977,408	238,045	110,908	2,326,361	
Hexamethylenetetramine Producers						
Borden, Inc.	Fayetteville, NC	63,000	9,000	18,000	90,000	1.30
W. R. Grace & Company	Nashua, NH	63,000	9,000	18,000	90,000	1.30
Occidental Petroleum Company	North Tonawanda, NY	52,500	7,500	15,000	75,000	1.08
Plastics Engineering Company	Sheboygan, WI	21,000	3,000	6,000	30,000	0.43
Tenneco, Inc.	Fords, NJ	42,000	6,000	12,000	60,000	0.86
Wright Chemical Corporation	Acme, NC	63,000	9,000	18,000	90,000	1.30
Total		304,500	43,500	87,000	435,000	
Trimethylolpropane Producers						
Celanese Corporation	Bishop, TX	5,050	757	757	6,565	0.09

TABLE E-46. FORMALDEHYDE EMISSIONS FROM CHEMICAL INTERMEDIATE USERS

Source: Systems Applications, Inc. 1982.

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NOTE: NUMERALS DENOTE NUMBER OF PLANTS.



Source: Systems Applications, Inc., 1980.

Storage and Transportation:

Pure formaldehyde is not available commercially because of its tendency to polymerize. It is sold as aqueous solutions containing from 37 to 50 percent formaldehyde by weight and varying amounts of methanol.

Should be protected against physical damage. Keep separate from oxidizing and alkaline materials. Indoor storage should be in storage areas having floors pitched toward a trapped drain or in curbed retention areas. Minimum storage temperatures to prevent polymerization range from 83°F for 37 percent formaldehyde containing 0.05 methyalcohol to 29°F for formaldehyde containing 15 percent methylalcohol. Shipped in insulated tank cars and tank trucks; 5- to 55-gallon metal drums, carboys, bottles, and tank barges.

Disposition:

Formaldehyde may be disposed of by incineration. Also, formaldehyde may be recovered from waste waters.

Sampling and Analytical Methods

- 1. NIOSH Method 3501
 - a. Liquid in bubbler (midget bubbler, 15-ml Girard T reagent).
 - b. Polarography.

Detection limit: 4.6 to 19.8 ppm for 18-liter samples.

Possible interferences:

Other volatile aldehydes such as acrylein, crotonaldehyde, benzaldehyde, and products diffusing out of polyvinyl chloride tubing may cause significant interference.

- 2. NIOSH Method 2502
 - a. Solid Sorbent Tube [2-(benzylamino) ethanol or Chromasorb 102 or XAD-2 120 mg/60 mg].
 - b. Gas chromatography.
 - c. Flame ionization detectors.

Detection limit:

0.25 to 4 ppm with 12-liter sample.

Possible interferences:

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Phenol has almost the same retention time. Acid mists may inactivate the sorbent, leading to inefficient collection of formaldehyde.

- 3. NIOSH Method 3500
 - a. Filter and impingers, 1µm PTFE membrane and two impingers, each with 20 ml 1 percent sodium bisulfite solution.
 - b. Visible absorption spectrophotometry.

Detection limit:

0.02 to 0.4 ppm for 80-liter sample

Possible interferences:

Phenols in 8:1 excess produce 10 to 20 percent bias. Ethanol and higher M.W. alcohols, olefins, aromatic hydrocarbons, and cyclohexanone produce small negative interferences. Little interference is seen from other aldehydes.

- 4. NIOSH Method 235
 - a. Alumina collection.
 - b. Methanol-water elution.
 - c. Spectrophotometric measurement.

Detection limit: 0.3 to 0.7 ppm in 6-liter sample

Possible interferences:

Saturated aldehydes give less than 0.01 percent positive interference. Phenols cause 10 to 20 percent negative interference when present in an 8:1 ratio over formaldehyde ethylene and propylene present in a 10:1 excess over formaldehyde give 5 to 10 percent negative interference, while 2-methyl-1,3-butadiene in a 15:1 excess over formaldehyde causes a 15 percent negative interference. Cyclohexanone causes a bleaching of the final color.

- 5. Method J (Appendix A)
 - a. Collection in dinitrophenyl hydrazine (DNPH).
 - b. Solvent extraction of DNPH derivitives.
 - c. Reversed phase high pressure liquid chromatography
- 6. Method K (Appendix A)
 - a. Collection in 1 percent sodium bisulfate impinger.
 - b. Determination of formaldehyde using chromotropic acid, acrolein, and mercuric chloride hexylrecorcinol with gas chromatography/flame ionization detection

Detection limit:

10 to 30 ppb 120-liter sample

Possible interferences:

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High levels of phenols, ethylene, and propylene cause negative interferences with formaldehyde.

Permissible Exposure Limits

OSHA		ACGIH	NIOSH		
TWA Ceiling Peak	3 ppm 5 ppm 10 ppm(30 min.)	2 ppm(3 mg/m ³)	1.2 mg/m³(30 min)		
Odor per-					

ception 1 ppm

The ACGIH has listed formaldehyde for intended changes to delete the ceiling, to add 1 ppm (1.5 mg/m³) for a TWA, to add 2 ppm (3 mg/m³) as an STEL, and to add a notation that formaldehyde is an industrial substance suspected of carcinogenic potential for man.

Human Toxicity

Acute Toxicity:

Irritant to skin, eyes, and mucous membrane. If swallowed, causes violent vomiting and diarrhea, which can lead to collapse. Frequent or prolonged exposure can cause hypersensitivity leading to contact dermatitis. Irritant to eyes at 20 ppm.

Chronic Toxicity:

After reviewing scientific data and public comments relevant to formaldehyde, EPA has determined there may be a reasonable basis to conclude that certain exposures to formaldehyde present or will present a significant risk of widespread harm to human beings from cancer.

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Chemical Name

Hexachlorocyclopentadiene

CAS Number

77-47-4

Chemical Classification

Chlorinated aromatic

Synonyms

C-56; 1,3-cyclopentadiene, 1,2,3,4,5,5 hexachloro-HCCPD; hexachlorcyklopentadien; hexachlorocyclopentadiene; NCI-C55607. perchlorocyclopentadiene.

Physical/Chemical Properties

Description: Pale yellow liquid; pungent odor. Boiling Point: 239°C Melting Point: -9.6°C Molecular Weight: 272.8 Chemical Formula: C_5Cl_6 Vapor Pressure: 0.4 mm Hg at 50°C; 7.5 mm Hg at 100°C Vapor Density: 9.42 (air = 1) Refractive Index: $N_{D}^{25} = 1.563$ Solubility: Not available Log Partition Coefficient (Octanol/water): 3.99 Photochemical Reactivity: Not available

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Chemical Reactivity:

When heated to decomposition, emits toxic fumes of chloride. Incompatible with sodium.

Environmental Fate

Important processes for the fate of HCCPD are near-surface photolysis, adsorption onto organic matter, and possible acid-catalyzed hydrolysis to tetrachlorocyclopentadiene if HCCPD is adsorbed onto a clay surface. HCCPD bioaccumulated in many organisms with weak biodegradation to tetrachlorocyclopentadienone hydrate occurring.

Source of Emissions

Production:

Mixed pentanes are chlorinated to polychlorinated pentanes in the liquid phase followed by vapor phase chlorinalysis and ring closure over a surface-active catalyst.

Uses:

Intermediate for resins, dyes, pesticides, fungicides, pharmaceuticals, and flame retardants.

Tables E-47 through E-51 and Figure E-4 present data on hexachlorocyclopantadiene production, consumption, and emissions.

Storage:

Sold as a distilled liquid of high purity in 55-gallon lined drums and in tank cars. Not corrosive to most materials of construction if moisture is rigorously excluded. To avoid possibility of iron contamination and corrosion, glass, nickel, or baked phenolic coatings are recommended.

Transportation:

Transported in lined 55-gallon drums or by tank car.

Disposition:

Hexachlorocyclopentadiene may be disposed of by incineration after it is mixed with another combustible fuel. Care must be taken to assure complete combustion to prevent the formation of phosgene. An acid scrubber is required to remove the halo-acids produced.

Sampling and Analytical Methods

- 1. NIOSH Method 308
 - a. Adsorption on Propak T.
 - b. Desorption with hexane.
 - c. Gas chromatography.

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d. Electron capture detector.

Source	Location	1978 Esti- mated produc- tion (10 ⁶ lb/yr)	1978 Esti- mated capacity (10 ⁶ lb/yr)	Geographic coordinates latitude/longitude
Hooker Chemical &	Montague, MI	1.75	NA ^b	43 24 45/86 22 30
Plastics Corp.	Niagara Falls, NY	3.50	NA	43 04 52/79 00 34
Velsicol Chemical Corporation	Memphis, TN	1.75	NA	35 09 50/90 57 45
Total		7	NA	

TABLE E-47. PRODUCTION OF HEXACHLOROCYCLOPENTADIENE

^aIndividual site production allocated by the ratio of the total number of employees at each site compared with the total number of employees at all three sites.

^bNot available.

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Source: Systems Applications, Inc. 1980.

Compound	End- use category	1974 production, 10 ⁶ lb	1978 Status	Known producer	Location
Aldrin	Pesticides	6.5	No longer made		
Chlorodane ·	Pesticide	21.2	N/A ^a	Velsicol	Marshall, IL
Dieldrin	Pesticide	1.0	No longer made		
Endosulfan	Pesticide	1.5	N/A	FMC & Hooker	New York, NY
Endrin	Pesticide	1.2	No longer made		
Heptachlor	Pesticide	2.0	N/A	Velsicol	Memphis, TN
Pentac ^R	Pesticide	N/A	No longer made		
Het-acid	Flame retardant	N/A	N/A	Hooker	Niagara Falls, NY
Mivex	Pesticide	N/A	No longer made		
Het-anhydride	Flame retardant	7.0	N/A	Hooker	Niagara Falls, NÝ
Dichlorane plus	Flame retardant	N/A	N/A	Hooker	Niagara Falls, NY
Chlorendic diesters	Resins	N/A	N/A	Velsicol	Memphis, TN

TABLE E-48. HEXACHLOROCYCLOPENTADIENE DERIVATIVES

^aNot available.

Source: Systems Applications Inc. 1980.

Company	Location	Process emissions		Storage emissions		Fugitive emissions		Total emissions	
		lb/yr	g/s	lb/yr	g/s	lb/yr	g/s	lb/yr	g/s
Hooker	Montague, MI Niagara Falls, NY	9,100 18,200	0.131 0.262	1,400 2,800	0.020 0.040	3,500 7,000	0.050 0.101	14,000 28,000	0.202
Velsicol	Memphis, TN	9,100	0.131	1,400	0.020	3,500	0.050	14,000	0.202
Total		36,400		5,600		14,000		56,000	

TABLE E-49. 1978 HEXACHLOROCYCLOPENTADIENE PRODUCTION EMISSIONS

Source: Systems Applications, Inc. 1980.

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			Geographic		Process Storage emissions emissions		Total emissions	
Company	Location	End-use ^a	latitude/longitude	lb/yr	lb/yr	lb/yr	lb/yr	g/s
Hooker	Montague, MI Niagara Falls, NY	А А, В	43 24 45/86 22 30 43 04 52/79 00 34	570 810	90 125	215 315	875 1,250	0.013 0.018
Velsicol	Memphis, TN Marshall, IL	B,C A	35 09 50/90 57 45 39 23 00/87 42 30	390 180	60 25	150 70	600 275	0.009 0.004
FMC	Middleport, NY	А	43 12 21/78 29 23	325	50	125	500	0.007
Tota	1			2,275	350	875	3,500	

TABLE E-50. 1978 HEXACHLOROCYCLOPENTADIENE END-USE EMISSIONS

^aEnd-use code: A - pesticide, B - flame retardant, C - resin.

Source: Systems Applications, Inc. 1982.

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				Stor D1	Dlanta	Source ^t type	Emissions g/s		
No.	Company	Site	Latitude/Longitude	station	type		Process	Storage	Fugitive
1	Hooker	_Montague, MI	43 24 45 086 22 30	14840	1	1 2	.131040 .008208	.020160 .001296	.050400 .003096
2	Hooker	Niagara Falls, NY	43 03 02 079 00 27	14747	1	1 2	.262080 .011664	.040320 .001800	.100800 .004536
3	Velsicol	Memphis, TN	35 09 50 089 57 45	13963	1	1 2	.131040 .005616	.020160 .000864	.050400 .002160
4	Velsicol	Marshall, IL	39 23 00 087 42 30	93819	2	2	.002592	.000360	.001008
5	FMC	Middleport, NY	43 12 21 078 29 23	14747	2	2	.004680	.000720	.001800

TABLE E-51. EMISSIONS AND METEOROLOGICAL STATIONS OF SPECIFIC POINT SOURCES OF HEXACHLOROPENTADIENE

^aPlant types. 1: Plant produces and consumes hexachlorocyclopentadiene; 2: Plant consumes hexachlorocyclopentadiene.

^bSource types: 1: Hexachlorocyclopentadiene production; 2: Hexachlorocyclopentadiene consumption.

Source: Systems Applications, Inc. 1982.



Figure E-4. Specific point sources of hexachlorocyclopentadiene emissions.

Source: Systems Applications, Inc. 1980.

	Detection limit: 25 ppt
	Possible interferences: Any compound with the same retention time as hexachlorocyclopentadiene at the operating conditions is an interferent.
2.	<pre>Method C (Appendix A): C₆C₁₂ hydrocarbons and other nonpolar organics with boiling point between 60° and 200°C. a. Adsorption on Tenax. b. Thermal desorption. c. Gas chromatography/mass spectrometry analysis.</pre>
	Detection limit: 1 to 200 ppt for a 20-liter sample
	Possible interferences: Blank levels usually limit sensitivity artifacts due to reactive components $(0_3, NO_x)$. Sample can be analyzed only once.
3.	 Method D (Appendix A): C₆-C₁₂ hydrocarbons and other nonpolar organics with boiling point of 60° to 200°C. a. Adsorption on Tenax. b. Thermal desorption into canister. c. Gas chromatography/flame ionization detection, or gas chromatography/mass spectrometry analysis.
	Detection limit: 0.01 to 1 ppb for a 20-liter sample
	Possible interferences: Blanks and artifact problems in Method C, above.
4.	 Method H (Appendix A) a. Adsorption on solid adsorbent such as polyurethane foam, XAD-2, or Chromasorb 102. b. Solvent desorption. c. Gas chromatography/electron capture detection, gas chro- matography/mass spectrometry, or gas chromatography/flame ionization detection analysis.
	Detection limit: 3 mg/m³ (1500 m³ sample)
	Possible interferences: None.

Permissible Exposure Limits

	OSHA	ACGIH	
TWA		0.01 ppm (0.1 mg/m ³)	_
STEL		0.03 ppm (0.3 mg/m ³)	

The ACGIH has listed hexachlorocyclopentadiene for intended changes to delete the STEL.

Human Toxicity

Acute Toxicity: A skin and eye irritant. High oral toxicity. Moderate skin irritant.

Chronic Toxicity: Selected by the National Toxicology Program for carcinogenesis bioassay as of January 1983.

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Chemical Name

Maleic anhydride

CAS Number

108-31-6

Chemical Classification

Anhydride (unsaturated)

Synonyms

Cis-butenedioic anhydride; 2,5-furandione; maleic acid anhydride; toxilic anhydride

Physical/Chemical Properties

Description: Colorless needles Boiling Point: 200°C Melting Point: 53°C Molecular Weight: 98.1 Chemical Formula: HC:CH C(0)OC(0)Vapor Pressure: 1 mm at 44°C Vapor Density: 3.4 (air = 1)Refractive Index: Not available Solubility: Soluble in water, acetone, alcohol, and dioxane; partially soluble in chloroform and benzene. Log Partition Coefficient (octanol/water): Not available Photochemical Reactivity: Not available

Chemical Reactivity:

Dust and vapors are very flammable in air. Reacts violently with alkali metals, amines, and other strong oxidizing agents. Incompatable with cations or bases. Will react with water or steam to produce heat.

Environmental Fate

Because of its high boiling point and solid state at ambient temperatures, most maleic anhydride emitted to the air is expected to precipitate and be solubilized in water. Conversion to maleic acid and subsequent biodegradation is likely to be a major pathway. Maleic anhydride in wastewater is easily decomposed by test-activated sludge.

Source of Emissions

Production:

Vapor phase oxidation of benzene in the presence of vanadium oxide catalyst Vapor phase oxidation of n-butane in the presence of a phosphorous-vanadium catalyst Recovery from phthalic anhydride production

Uses:

Used exclusively as an intermediate to make: Unsaturated polyester resins Agricultural chemicals Lubricating oil additives Copolymers Fumaric acid Malic acid Chlorendic acid and anhydride Alkyd resins

Tables E-52 and E-53 present maleic anhydride production and consumption data.

Storage:

Should be protected from physical damage and stored in a cool, dry, well-ventilated area away from ignition sources; outside or detached storage is preferred. Should be protected from moisture and stored separately from alkali metals, amines, and other strong oxidizing agents. Keep away from flame or spark as dust and vapor for molten product are very flammable.

Transportation:

Shipped in fiber drums (rod, flake, and lump); iron drums (fused); and tank cars (molten).

Company	Location	Annual Capacity, 10 ⁶ lb	Raw material and remarks
Ashland Oil, Inc. Ashland Chem. Co., Div. Petrochems. Div. Denka Chem. Corp.	Neal, W.Va. Houston, Tex.	50 50	n-Butane n-Butane
Monsanto Co. Monsanto Indust. Chems. Co.	Pensacola, Fla. St. Louis, Mo.	130 110	n-Butane n-Butane (40%); benzene (60%); plant will be con- verted to 100% bu- tane raw material.
Standard Oil Co. (Indiana) Amoco Chems. Corp., subsid. United States Steel	Joliet, Ill.	60	n-Butane
Uorp. USS Chems., div.	Neville Island, Pa.	70	n-Butane (45%); benzene (55%); plant is being con- verted to 100% bu- tane based feed- stock; benzene based capacity is on standby.
	TOTAL	470	

TABLE E-52. PRODUCTION OF MALEIC ANHYDRIDE

Source: SRI International. 1985.

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Use	Millions of pounds (1978)	Percent of total consumption
Unsaturated polyester resins Agricultural chemicals Lubricating oil additives Copolymers Fumaric acid Malic acid Chlorendic acid and anhydride Alkyd resins All other	180 31 30 20 20 15 6 5 24	54 9 6 6 5 2 2 7
TOTAL	331	100

TABLE E-53. USES OF MALEIC ANHYDRIDE

Source: U.S. EPA 1981 (CHIP)

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Disposition:

Maleic anhydride may be disposed of by controlled incineration. Care must be taken to assure complete oxidation to non-toxic products.

Sampling and Analytical Methods

- 1. NIOSH Method 302
 - a. Bubbler collection.
 - b. High-pressure liquid chromatography.

Detection limit: 10 ppb with a 360-liter sample

Possible interferences: Any compound that has the same retention time as maleic acid at the process conditions is an interferent. Maleic anhydride is immediately hydrolized to maleic acid upon collection. This method will not differentiate between maleic acid and maleic anhydride.

Permissible Exposure Limits

TWA

OSHA ACGIH 0.25 ppm (1 mg/m³) 0.25 ppm (1 mg/m³)

Human Toxicity

Acute Toxicity: An eye irritant. Irritation to skin, eyes, and mucous membranes. Inhalation of vapor can cause pulmonary edema. Causes burns to skin and eyes.

Chronic Toxicity: Has been found to be an equivocal tumorigenic agent in rats. In one study one rat developed two fibrosarcomas at the site of injection. A mutagenicity test on Chinese hamster cells was positive for chromosomal aberrations.

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Chemical Name

Manganese

CAS Number

7439-96-5

Chemical Classification

Metallic element

Synonyms

Colloidal manganese; mangan

Physical/Chemical Properties

Description: Of the four allotropic forms, alpha is the most important. Brittle reddish-gray, silvery metal. Boiling Point: 2097°C Melting Point: 1245°C Molecular Weight: 54.9 Chemical Formula: Mn Vapor Pressure: 1 mm at 1292°C Density: 7.20 Refractive Index: Not available Solubility: Decomposes in water; readily dissolves in dilute mineral acid. Log Partition Coefficient (octanol/water): Not available Photochemical Reactivity: No atmospheric transformation (aerosol and particle deposition). Reacts with all mineral acids with evolution of hydrogen and formation of divalent manganous salts.

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Chemical Reactivity:

Will react with water or steam to produce hydrogen. Can react with oxidizing materials. Superficially oxidizes on exposure to air. Burns with an intense white light when heated in air.

Environmental Fate

Manganese in the ecosystem has well-established lines of movement from rocks to soils to plants to animals, from soils to water to organisms, and back to water and soils. Marine organisms can concentrate manganese in their bodies, and man retains manganese at a concentration 3 to 4 times that in his food.

Source of Emissions

Production:

Reduction of the oxide with aluminum or carbon. Obtained electrolytically from sulfate or chloride solution.

Uses:

Ferroalloys (steel manufacture) Nonferrous alloys (improved corrosion resistance and hardness) High purity salt for various chemical uses Purifying and scavenging agent in metal production Manufacture of aluminum by Toth process

Tables E-54 through E-60 present manganese consumption and emission data.

Storage:

Protect containers against physical damage. Food and drinks should be kept out of work area.

Transportation:

Shipped in drums and in car lots in pure, electrolytic, or powdered grades

Disposition:

Manganese may be disposed of by sanitary landfill.

Sampling and Analytical Methods

- 1. NIOSH Method 173
 - a. Filter collection.

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- b. Acid digestion.
- c. AAS (atomic absorption spectrophotometry).

Detection limit: 0.2 mg/m³ with a 3-liter sample

Use	Usage, %	Manganese ore consumed, tons/yr
Manganese alloys/metals	79	1,263,581
Pig iron and steel	9	143,761
Dry cells, chemicals, misc.	12	193,581
Total	100	1,600,923

TABLE E-54. UNITED STATES MANGANESE ORE CONSUMPTION

Source: Systems Applications, Inc. 1980.

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Source	Nationwide emissions, lb/yr
Mining	Negligible
Iron and steel	9,212,000
Gray iron foundry	5,540,000
Ferro alloy, ferro manganese, silico manganese	12,632,000
Chemical applications	644,000
Battery production	276,000
Welding rod manufacture	48,000
Power plants	
Coal Oil	5,280,000 13,566
Industrial Boilers	
Coal Oil	352,000 14,091
Residential/commercial	
Coal Oil	16,000 4,454
Coke ovens	1,950,000
Total	35,982,111

TABLE E-55. 1978 NATIONWIDE MANGANESE EMISSIONS

Source: Systems Applications, Inc. 1980.

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		Manganese	Average emissions per site	
Region	Number of sites	emissions, lb/yr	lb/yr	g/s
New England	10	55,045	5,505	0.079
Middle Atlantic	65	2,846,685	43,795	0.630
East North Central	84	3,859,795	45,950	0.661
West North Central	5	101,260	20,250	0.292
South Atlantic	22	819,940	37,270	0.537
East South Central	25	626,250	25,050	0.361
West South Central	12	211,865	17,655	0.254
Mountain	2	221,210	110,605	1.592
Pacific	32	469,950	14,685	0.211
Total	257	9,212,000	35,844	

TABLE E-56. MANGANESE EMISSIONS FROM IRON AND STEEL PRODUCTION

Source: Systems Applications, Inc. 1980.

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		Manganese	Average emissions per site	
Region	Number of sites	emissions, 1b/yr	lb/yr	g/s
New England	13	138,500	10,655	0.15
Middle Atlantic	42	508,985	12,120	0.17
East North Central	129	2,887,725	22,385	0.32
West North Central	29	315,085	10,865	0.16
South Atlantic	22	408,575	18,570	0.27
East South Central	37	654,410	17,685	0.25
West South Central	19	277,000	14,580	0.21
Mountain	5	65,785	13,157	0.19
Pacific	28	283,925	10,140	0.15
Total	324	5,540,000	17,100	

TABLE E-57. MANGANESE EMISSIONS FROM GRAY IRON FOUNDRY OPERATIONS

Source: Systems Applications, Inc. 1980.

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Region	Number of sites	Manganese emissions lb/yr
New England	0	0
Middle Atlantic	12	2,972,220
East North Central	8	1,981,480
West North Central	1	247,685
South Atlantic	8	1,981,480
East South Central	13	3,219,905
West South Central	1	247,685
Mountain	4	990,740
Pacific	4	990,740
Total	51	12,632,000

TABLE E-58. MANGANESE EMISSIONS FROM FERROALLOY, FERRO MANGANESE, AND SILICA MANGANESE PRODUCTION

Source: Systems Applications, Inc. 1980.

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		Manganese	Average emissions per site	
Region	Number of sites	sites lb/yr	lb/yr	g/s
New England	9	36,960	4,105	0.06
Middle Atlantic	51	596,640	11,700	0.17
East North Central	156	1,789,920	11,475	0.17
West North Central	111	496,320	4,470	0.07
South Atlantic	61	1,034,880	16,965	0.25
East South Central	44	860,640	19,560	0.29
West South Central	3	68,640	22,880	0.33
Mountain	38	359,040	9,450	0.14
Pacific	1	36,960	36,960	0.54
Total	474	5,280,000	11,140	

TABLE E-59. MANGANESE EMISSIONS FROM ELECTRICAL UTILITY POWER PLANTS (coal-fired)

Source: Systems Applications, Inc. 1980.

Region	Number of sites	Manganese emissions, lb/yr
New England	0	0
Middle Atlantic	15	479,505
East North Central	25	799,185
West North Central	3	95,900
South Atlantic	4	127,870
East South Central	9	287 ,7 05
West South Central	2	63,935
Mountain	2	63,935
Pacific	1	31,965
Total	61	1,950,000

TABLE E-60. MANGANESE EMISSIONS FROM COKE OVEN OPERATIONS

Source: Systems Applications, Inc. 1980.

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Possible interferences:

Spectral interferences; background or nonspecific absorption; ionization interferences, chemical interferences; and physical interferences.

- 2. NIOSH Method 351
 - a. Filter collection.
 - b. Acid digestion.
 - c. Inductively coupled plasma-atomic emission spectroscopy analysis.

Detection limit:

5 to 2000 μ g/m³ with a 5-liter sample.

Possible interferences: Physical interferences; chemical interferences; spectral interferences.

3. NIOSH Method S5

- a. Filter collection.
- b. Acid digestion.
- c. Atomic absorption.
- Detection limit: 0.2 to 20 mg/m³ with a 22.5-liter sample.

Possible interferences: No known interferences.

Permissible Exposure Limits

	OSHA	ACGIH
TWA	<u> </u>	1 mg/m ³ (fume)
STEL		3 mg/m³ (fume)
Ceiling	5 mg/m³	5 mg/m^3 (dust and com-
-	_	pounds)

Human Toxicity

Acute Toxicity:

Occurs by inhalation of the dust or fumes. Symptoms are languor, sleepiness, weakness, emotional disturbances, spastic gait, and paralysis.

Chronic Toxicity:

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Chronic manganese poisoning is a clearly characterized disease that results from the inhalation of fumes or dusts of manganese. Exposure to heavy concentrations for as little as three months may produce the condition, but it usually develops after 1 to 3 years of exposure. The central nervous system is the chief site of damage. Manganese has also been found to be an equivocal tumorigenic agent in rats. Bibliography

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Chemical Name

Mercury

CAS Number

7439-97-6

Chemical Classification

Metallic element

Synonyms

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Colloidal mercury; kwik; mercure; mercurio; mercury-metallic (DOT);
metallic mercury; NCI-C60399; quecksilber; quicksilver; RTEC
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Physical/Chemical Properties

Description: Silvery, extremely heavy liquid, sometimes found native. Boiling Point: 356.6°C Melting Point: -38.85°C Molecular Weight: 200.6 Chemical Formula: Hg Vapor Pressure: 1 mm at 126.2°C; 2 x 10⁻³ mm at 25°C Density: 13.54 g/ml (20°C) **Refractive Index:** Not available Solubility: Insoluble in HCl; soluble in sulfuric acid upon boiling; readily soluble in nitric acid; insoluble in water, alcohol, and ether; soluble in lipids. Log Partition Coefficient (octanol/water): Not available

Photochemical Reactivity: Not photochemically reactive

Chemical Reactivity:

Incompatible with acetylenic compounds, ammonia, boron diiodophosphide, ethylene oxide, metals, methyl azide, methylsilane, oxygen, oxidants, and tetracarbonylnickel.

Environmental Fate

Breakdown of atmospheric dimethyl mercury is of slight importance. Oxidation of metallic mercury forms ionic mercury; reduction forms an HgS precipitate. Metallic Hg, methylated Hg, and adsorbed Hg all volatilize. Mercury is adsorbed by most particles, buried in sediment, and reduced to HgS. It is bioaccumulated by all organisms and readily methylated metabolically.

Source of Emissions

Production:

By heating cinnabar in air, or with lime, and condensing the vapor. Purified by distillation. In 1982 and 1983, Nevada was the only mercury-producing State. Producers were the Carlin gold mine, the Pinson gold mine, and the McDermitt mercury mine. During 1983, four companies specialized in processing primary or scrap mercury: Bethlehem Apparatus Co., Hellertown, PA; D.F. Goldsmith Chemical & Metal Corp., Evanston, IL; Mercury Refining Co., Inc., Albany, NY; and Troy Chemical Corp., Newark, NJ.

Uses:

Manufacturing of all mercury salts Mercury cells Electric switches Propellant Mercury vapor lamps Barometers Thermometers Medicine Amalgams Mercury boilers

Tables E-61 and E-62 present mercury production and consumption data.

Storage:

Containers should be kept closed. Preferably, small quantities should be stored in a polyethylene bottle, and the mercury surface should be covered with water to prevent evaporation as much as possible.

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	1979	1980	1981	1982	1983
Producing mines	3	4	3	3	3
Mine production	29,519	30,657	27,904	25,760	25,070
Secondary production Industry Government Industry stocks, year end Shipments from the Nation- al Defense Stockpile	4,287 11,300 27,582 196	6,793 10,013 33,069 -	4,244 7,000 27,339 -	4,473 - 29,327 7,088	13,474 - 31,518 6,000
Imports for consumption	26,448	9,416	12,408	8,916	12,786
Consumption, reported	62,205	58,983	59,244	48,943	49,138
Consumption, apparent	82,721	51,392	57,286	44,249	55,252

TABLE E-61. MERCURY PRODUCTION (flasks)

Source: Minerals Yearbook.

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SIC code	Use	1979	1980	19 81	1982	1983
28 2812	Chemical and allied products: Chlorine and caustic soda	12,180	9,470	7,323	6,243	8,054
2816 2819 2821 2819 2851 2851 2879 -	Pigments Catalysts, miscellaneous Catalysts for plastics Laboratory uses Paints Agricultural chemicals Other chemicals and allied products	W ^a 1,257 .W 410 9,979 W 82	W 765 W 363 8,621 W W	W 815 W 328 7,049 79 W	W 499 W 281 6,794 36 W	W 484 W 280 6,047 W W
36 3641 3643 3692 -	Electrical and electronic uses: Electric lighting Wiring devices and switches Batteries Other electrical and elec- tronic uses	511 3,213 25,299 106	1,036 3,062 27,829 144	1,043 2,641 29,441 W	826 2,004 24,880 W	1,273 2,316 23,350 W
38	Instruments and related products:					
382	Measuring and control in-	3,603	3,049	5,671	3,064	2,465
3 843	Dental equipment and sup-	1,422	1,779	1,613	1,019	1,597
-	Other instruments and re- lated products	192	190	253	194	W
-	Other	556	790	242	984	1,356
	Total	62,205	58,983	59,244	48,943	49,138

TABLE E-62. MERCURY CONSUMED IN THE UNITED STATES, BY USE (flasks)

^a W = Withheld to avoid disclosing company proprietary data; included in "Total".

Source: Minerals Yearbook.

Transportation: Transported in 1-, 5-, and 10-pound bottles and 76-pound flasks.

Disposition:

Elemental mercury may be accumulated for sale or for purification and reuse. Inorganic mercury (mercuric chloride, mercuric nitrate, mercuric sulfate) may be disposed of by incineration followed by recovery/removal of mercury from the gas stream. Alternatively, mercury compounds may be recovered from brines, sludges, and spent catalysts. Mercury in inaccessible locations (cracks, etc.) can be treated with calcium polysulfide and excess sulfur.

Sampling and Analytical Methods

NIOSH Method

 a. Solid Sorbent Tube (30 mg silvered chromosorb P, with glass-fiber prefilter.
 b. Automatic absorption, flameless.

Detection limit: 0.3 ppb per 3-liter sample

Possible interferences:

Chlorine, along with other oxidizing gasess, will attack silver. Methyl mercuric chloride is a potential interferent.

Permissible Exposure Limits

	OSHA	ACGIH (skin)	NIOSH
TWA		0.05 mg/m ³ air (all forms ex-	0.05 mg/m ³
		cept alkyl vapor)	
		0.1 mg/m ³ (ary] and inorganic	
		compounds)	
		0.01 mg/m ³ (alkyl compounds)	
Ceiling	1 mg/10m³	0.03 mg/m³ (alkyl compounds)	

Human Toxicity

Acute Toxicity:

Gastrointestinal tract effects, central nervous system effects. High toxicity inhalation. A general protoplasmic poison after absorption, it circulates in the blood and is stored in the liver, kidneys, spleen, and bone. Solution salts have violent corrosive effects on skin and mucous membranes, severe nausea, vomiting, abdominal pain, bloody diarrhea, kidney damage; death usually occurs within 10 days.

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Chronic Toxicity:

Mercury has a cumulative effect and has a tendency to deposit in certain organs; most notably the brain, liver, and kidneys, although it can be found in nearly all tissues. The TLV is set at a point to prevent chronic poisoning. The onset of symptoms of mercury toxicity from chronic exposure may be ignored by the individual or attributed to other causes. This is particularly true with erethism, which is characterized by irritability, outbursts of temper, excitability, shyness, resentment of criticism, headache, fatigue, and indecision.

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Chemical Name

Methylene chloride

CAS Number

75-09-2

Chemical Classification

Chlorinated hydrocarbon

Synonyms

Aerothene MM; chlorure de methylene; DCM; dichloromethane; dichloromethane (DOT); freon 30; methane dichloride; methylene bichloride; methylne chloride; methylene chloride (DOT); methylene dichloride; metylenu chlorek; narkotil; NCI-C50102; solaesthin; solmethine

Physical/Chemical Properties

Description: Colorless volatile liquid; penetrating ether-like odor.
Boiling Point: 40.1°C
Melting Point: -97°C
Molecular Weight: 84.9
Chemical Formula: CH ₂ Cl ₂
Vapor Pressure: 380 mm at 22°C
Vapor Density: 2.93 (air = 1)
Refractive Index: N _D ²⁰ = 1.4242
Solubility: Soluble in alcohol and ether; slightly soluble in water.
Log Partition Coefficient (octanol/water): 1.25

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Photochemical Reactivity:

Reactivity toward OH. is a half-life of approximately 1 year, less than methane. No reaction toward O_3 .

Chemical Reactivity:

When heated to decomposition, emits highly toxic fumes of phosgene. Not explosive under ordinary conditions, but will form explosive mixtures in atmosphere having high oxygen content or in liquid O_2 , N_2O_4 , K, Na, NaK. Reacts violently with Li, NaK, potassium-tert-butoxide, and (KOH+n-methyl-nnitrosourea).

Environmental Fate

Because of high vapor pressure, volatilization to the atmosphere is rapid and is a major transport process. In tetrosphere, oxidation by hydroxyl radicals to carbon dioxide, carbon monoxide, and phosgene is important fate mechanism.

Source of Emissions

Production/processing:

Chlorination of methyl chloride and subsequent distillation. Chlorination of methane and subsequent distillation.

Uses:

Aerosal products Paint removers Solvent degreasing Plastics processing Blowing agent in foams Polycarbonate resins Solvent in inks. adhesives

Solvent for triacetate extrusion Solvent in the pharmaceutical and electronics industry Photographic film Cleaning uses

Tables E-63 through E-67 present methylene chloride production, consumption, and emission data.

Storage:

Should be protected against physical damage and stored in a cool, dry, well-ventilated location, away from any area where the fire hazard may be acute.

Transport:

Should be shipped in glass bottles, 5- and 55-gallon drums, tank cars, and tank trucks.

Disposition:

Methylene chloride may be disposed of by incineration after mixing with another combustible fuel; care must be exercised to assure complete combustion to prevent the formation of phosgene. An acid scrubber is necessary to remove the halo acids produced.

Company .	Location	1978 estimated production, ^a 10 ⁶ lb/yr	Process ^b	1978 estimated capacity, 10 ⁶ 1b/yr	Geographical location, latitude/longitude
Allied Chemical Corp.	Moundsville, WV	31	A,B ^C	50	39 54 24/80 47 51
Diamond Shamrock	Belle, WV	63	А	100	38 14 09/81 32 38
Dow Chemical	Freeport, TX Plaquemine, LA	125 112	B A	200 180	28 59 15/95 24 45 30 19 00/91 15 00
Stauffer	Louisville, KY	38	A	60	38 12 09/85 51 49
Vulcan Materials Co.	Geismar, LA Wichita, KS	50 106	A A,B ^d	80 170	30 10 00/90 59 00 37 36 55/97 18 30
Total		525		840	

TABLE E-63. PRODUCTION OF METHYLENE CHLORIDE

^a Distribution of the 525 million pounds per year for each producing location has been made as a direct ratio of total production/total capacity x individual plant capacity.

b (A) - Methanol hydrochlorination process or methyl chloride chlorination process.
 (B) - Methane chlorination process.

 $^{\rm C}$ 5% methane chlorination, 95% methyl chloride chlorination.

d 10% methane chlorination, 90% methyl chloride chlorination.

Source: Systems Applications, Inc. 1980.

End use	Percent of total consumption	End use consumption, 10 ⁶ lb/yr
Paint and varnish remover Metal degreasing Aerosols Plastics processing Export Miscellaneous	30 22 17 5 21 5	157.5 115.5 89.25 26.25 110.25 26.25
Total	100	525

TABLE E-64. 1978 METHYLENE CHLORIDE CONSUMPTION BY END USE

Source: Systems Applications, Inc. 1980.

TABLE E-65. 1978 METHYLENE CHLORIDE NATIONWIDE EMISSION LOSSES

End use	Estimated national emission, 10 ⁶ lb/yr
Production Paint and varnish remover Metal degreasing Aerosols Plastics processing Miscellaneous Export	0.65 157.5 107.1 89.25 26.25 26.25 0
Total	407.00

Source: Systems Applications, Inc. 1982.

		Process Storage vent emissions vent emissions		Fugitive emissions		Total emissions			
Company	Location	lb/yr	g/s	lb/yr	g/s	lb/yr	g/s	lb/yr	g/s
Allied Chemical	Moundsville, WV	980	0.014	74,030	1.066	14,430	0.208	89,440	1.288
Diamond Shamrock	Belle, WV	164	0.002	15 ,49 8	0.223	2,980	0.043	18,642	0.268
Dow Chemical	Freeport, TX Plaquemine, LA	16,353 234	0.235 0.003	119,566 22,178	1.720 0.319	37,780 4,268	0.543 0.061	173,699 26,680	2.498 0.383
Stauffer	Louisville, KY	990	0.014	93,480	1.346	17,970	0.259	112,440	1.619
Vulcan	Geismar, LA Wichita, KA	1,300 3,960	0.019 0.057	123,000 24,553	1.771 0.353	23,650 48,550	0.340 0.699	147,950 77,063	2.130
Total		23,981		472,305		149,628		645,914	

TABLE E-66. 1978 METHYLENE CHLORIDE PRODUCTION EMISSIONS

Source: Systems Applications, Inc. 1980.

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Cold cleaning		Open-top vapor c	legreasing	Conveyorized vapor degreasing		
Emissions/site, gm/s	Number of sites	Emissions/site, gm/s	Number of sites	Emissions/site, gm/s	Number of sites	
0.00952 0.00952 0.00952	7,284 18,892 32,084	0.288 0.288 0.288	82 170 257	0.857 0.857 0.857	14 30 50	
0.00952 0.00952	10,624 14,620 7,168	0,288 0,288 0,288	66 69 39	0.857 0.857 0.857	10 10	
0.00952	11,764 4,397 14 347	0.288	59 26 132	0.857 0.857 0.857	8 3 20	
	Cold clean Emissions/site, gm/s 0.00952 0.00952 0.00952 0.00952 0.00952 0.00952 0.00952 0.00952 0.00952 0.00952 0.00952	Cold cleaningEmissions/site, gm/sNumber of sites0.009527,2840.0095218,8920.0095232,0840.0095210,6240.0095214,6200.009527,1680.0095211,7640.009524,3970.0095214,347	Cold cleaningOpen-top vapor ofEmissions/site, gm/sNumber of sitesEmissions/site, gm/s0.009527,2840.2880.0095218,8920.2880.0095232,0840.2880.0095210,6240.2880.0095214,6200.2880.009527,1680.2880.0095211,7640.2880.0095211,7640.2880.0095214,3970.288	Cold cleaningOpen-top vapor degreasingEmissions/site, gm/sNumber of sitesEmissions/site, gm/sNumber of sites0.009527,2840.288820.0095218,8920.2881700.0095232,0840.2882570.0095210,6240.288660.0095214,6200.288690.009527,1680.288390.0095211,7640.288590.0095214,3470.288132	Cold cleaning Open-top vapor degreasing Conveyoriz vapor degrea Emissions/site, gm/s Number of sites Emissions/site, gm/s Emissions/site, of sites Emissions/site, gm/s 0.00952 7,284 0.288 82 0.857 0.00952 18,892 0.288 170 0.857 0.00952 32,084 0.288 257 0.857 0.00952 10,624 0.288 66 0.857 0.00952 14,620 0.288 39 0.857 0.00952 11,764 0.288 59 0.857 0.00952 11,764 0.288 26 0.857 0.00952 14,347 0.288 132 0.857	

TABLE E-67. EMISSIONS RATES AND NUMBER OF GENERAL POINT SOURCES OF METHYLENE CHLORIDE

Source: Systems Applications, Inc. 1980.

Sampling and Analytical Methods

- 1. NIOSH Method S329
 - a. Adsorption on charcoal.
 - b. Desorption with carbon disulfide.
 - c. Gas chromatography.

Detection limit: 350 to 10,400 mg/m³ (100-3000 ppm) per 1-liter sample

Possible interferences: High humidity will lower vapor trapping efficiency. Any compound with the same retention time as methylene chloride may be an interferent.

- 2. NIOSH Method P&CAM 127
 - a. Adsorption on charcoal.
 - b. Desorption with carbon disulfide.
 - c. Gas chromatography.

Detection limit: 0.05 mg/sample (0.01 ppm); minimum 0.5-liter sample

Possible interferences:

High humidity will lower vapor trapping efficiency. Any compound with the same retention time as methylene chloride may be an interferent.

- NIOSH Method 1005 (replaces NIOSH Methods S329 and P&CAM 127)
 a. Solid sorbent tube (two coconut shell charcoal tubes; 100
 - mg/50 mg).
 - b. Gas chromatography.
 - c. Flame ionization detector.

Detection limit: 3.0 ppm per 1-liter sample

Possible interferences: None identified.

- 4. Method B (Appendix A) C_2-C_{18} hydrocarbons and other nonpolar organics with a boiling point of 100° to 175°C.
 - a. Whole air collection in canister.
 - b. Cryogenic concentration.
 - c. Gas chromatography/flame ionization detection.

Detection limit:

0.1 ppb per 100-ml sample

Possible interferences:

Storage times greater than a week are not recommended. Laboratory contamination with methylene chloride is a common problem.
- 5. Method F (Appendix A) nonpolar volatiles with a boiling point 0° to 100°C.
 - a. Adsorption on carbon molecular sieves.
 - b. Thermal desorption into canister.
 - c. Analysis by gas chromatography/flame ionization detection or gas chromatography/mass spectrometry analysis.

Detection limit: 0.01-1 ppb per 20-liter sample

Possible interferences:

High temperature (350°C) required for desorption may decompose compounds. Laboratory contamination with methylene chloride is a common problem.

Permissible Exposure Limits

	OSHA	ACGIH
TWA	500 ppm	100 ppm (350 mg/m ³)
STEL		500 ppm (1740 mg/m ³)
Ceiling	1000 ppm	
Peak	2000 ppm (5 min. in 2 h)	

The ACGIH has listed methylene chloride for intended changes to delete the STEL.

Odor perception 25 to 50 ppm.

Human Toxicity

Acute toxicity:

Very dangerous to the eyes. Except for its property of inducing narcosis, it has very few other acute toxicity effects. Can be decomposed by contact with hot surfaces or open flame, which yields toxic fumes that are irritating. Can cause dermatitis upon prolonged skin contact.

Chronic Toxicity:

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EPA is awaiting the results of a National Toxicology Program peer review of a methylene chloride bioassay (February 1985). Preliminary findings of the bioassay are that methylene chloride is carcinogenic to laboratory animals.

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Chemical Name

4,4-Methylenedianiline

CAS Number

101-77-9

Chemical Classification

Aromatic Amine

Synonyms

4-(4-aminobenzyl) aniline; bis-p-aminofenylmethan; bis(p-aminophenyl) methane; bis(4-aminophenyl) methan; DADPM; DAPM; DDM; P,P'-diaminofenylmethan; 4,4'-diaminodiphenylmethan; diaminodiphenylmethane; P,P'-diaminodiphenylmethane; 4,4'-diaminodiphenylmethane; di-(4aminophenyl) methane; dianalinemethane, dianilinomethane, 4,4'diphenylmethanediamire; EPICURE DDM; HT 972; MDA; methylenebis (aniline); 4,4'-methylenebisaniline; methylenedianiline; p,p'methylenedianiline; 4,4'-methylenedianiline; TONOX.

Physical/Chemical Properties

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Description:
     Crystals from water or benzene; tan flakes or lumps, faint
     amine-like odor.
Boiling Point:
     398° to 399°C
Melting Point:
92° to 93°C
Molecular Weight:
     198.3
Chemical Formula:
     H_2NC_6H_4CH_2C_6H_4NH_2
Vapor Pressure:
     Negligible (0.2 mm Hg for one form)
Density:
     1.056 g/m<sup>3</sup> (liquid at 100^{\circ}C)
Refractive Index:
     Not available
Solubility:
      Slightly soluble in cold water. Very soluble in alcohol,
      benzene, ether.
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Log Partition Coefficient (octanol/water): Estimated between 1.8 and 2.5

Photochemical Reactivity:

No primary information is available, but the known photochemical reactivity of both toluene and aniline suggests that MDA may also be reactive.

Chemical Reactivity:

Weak base; has the general characteristics of primary aromatic amines. Most reactions involve substitution of the amine hydrogens or aromatic hydrogens. In some cases, the functional groups are totally altered. Polymers are formed when the amine is condensed with multifunctional reactants. Decomposes to highly toxic fumes of aniline and NO_v.

Environmental Fate

Only limited information is available on the chemical and biological transformation of MDA in the environment. MDA appears to undergo reactions typical of both aromatic amines and aromatic compounds in general. The low vapor pressure of MDA crystals make it improbable that MDA molecules evaporate readily to the atmosphere. No information was found to indicate bioaccumulation of MDA.

Source of Emissions

Production:

Acid catalyzed reaction of aniline with formaldehyde.

Uses:

Ninety-nine percent is consumed to manufacture methylene phenyl diisocyanate (MDI).

Other uses include epoxy and urethane curing, production of ketamines, wire coatings, circuit board coatings, dye intermediates, rubber processing chemicals, pharmaceuticals, and herbicides.

Tables E-68 and E-69 present MDA production and consumption data.

Storage:

Sold as a viscous liquid or lump in the crude form or as flakes or granules in the pure form. Stored in tanks, 55gallon drums, bags, or kegs. Generally, containers consist of fibrous material.

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TABLE E-68. PRESENT AND PROPOSED MDA MANUFACTURING PLANTS

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Company	Plant location	Comments
BASF Wyandotte Corp.	Parsippany, NJ Geismar, LA	Presently imports MDA. Had a 1977 capacity of less than 100,000 pounds/year. New plant scheduled for operation by 1985 with a capacity of 120 million pounds/year.
E.I. du Pont de Nemours	Belle, WV	Between 10 and 15 million pounds of MDA produc- tion in 1977. All production used to prepare Du Pont Spandex fibers and Quiana resins. Qiana resins no longer produced using MDA.
Mobay Chemical Corp.	New Martinsville, WV Baytown, TX	All MDA consumed onsite to produce MDI. The 1980 production capacities were 79 million pounds/year at each facility. The Baytown plant is scheduled to double its capacity by 1985.
Olin Corp.	Moundsville, WV (formerly Allied)	Olin does not produce MDI and is the only sup- plier of pure MDA. The 1972-73 production was approximately 2 million pounds.
Rubicon Chemicals Inc.	Geismar, LA	Most MDA is used to produce MDI. Present MDA capac- ity is approximately 79 million pounds/year. Expan- sion is planned to increase MDA capacity to 200 mil- lion pounds/year by 1985.
Uniroyal, Inc.	Naugatuck, CT	Polymeric MDA available as Tonox. MDA capacity unknown.
Upjohn Co.	La Porte, TX	Most MDA is used to produce MDI. MDA capacity in 1980 was 213 million pounds/year.

Note: ARCO chemical has a plant scheduled for operation in 1985 to produce MDI by a process that does not use MDA as an intermediate. MDI capacity 150 million pounds/year.

Source: PEI Associates, Inc. 1983.

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End-use application	Estimated pounds/ year of pure MDA	Estimated pounds/ year of polymeric MDA
Epoxy curing	200,000-450,000	1,500,000
Urethane curing	50,000	a
Ketamine production	40,000	a
Wire coating production	220,000	a
Production of coatings for printed circuit boards and aircraft parts	50,000	a
Dye intermediates	50,000	a
Rubber processing chemical	10,000	b
Corrosion inhibitor	0	a
Antioxidant for lubricating oil	0	200,000
Intermediate for pharmaceuticals, herbicides, etc.	140,000	a

TABLE E-69. ESTIMATED CONSUMPTION OF MDA FOR NON-MDI USES

^a No information found.

^b Although no estimate was reported, it is believed that some polymeric MDA is used for this purpose.

Source: PEI Associates, Inc. 1983.

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Transportation:

Shipped in bulk by tank car or in packaged container by truck. No special handling procedures.

Disposition:

Ninety-nine plus percent is consumed in chemical reactions. Any unreacted or spilled material is probably disposed of in a sanitary landfill.

Sampling and Analytical Methods

Limited information regarding sampling and analytical methods for MDA was reported by JRB Associates (1981). Adsorption onto activated charcoal, XAD-2, and XAD-4 was reported for aqueous solutions. No references were found for vapor monitoring of MDA. Analyses by liquid chromatography, visible spectrometry, and wet chemical methods have been reported. No data on any monitoring of MDA in the environment could be found.

Permissible Exposure Limits

	OSHA	ACGIH (skin)
TWA	Not established	0.1 ppm (0.8 mg/m ³)
STEL		0.5 ppm (4 mg/m^3)

The ACGIH has listed MDA for intended changes to delete the STEL and add notation that MDA is an industrial substance suspected of carcinogenic potential in man.

Human Toxicity

Acute Toxicity:

An eye irritant. Human systemic effects. High toxicity via oral, subcutaneous, and intraperitoneal routes. Does not seem to be readily absorbed through the skin.

Chronic Toxicity:

MDA has been shown to be carcinogenic in both sexes of rats and mice in bioassays conducted by the National Toxicology Program and is considered a potential carcinogen in humans.

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Chemical Name

Perchloroethylene

CAS Number

127-18-4

Chemical Classification

Chlorinated hydrocarbon (unsaturated)

Synonyms

Ankilostin; antisol 1; carbon bichloride; carbon dichloride; czterochloroetylen; didakene; dow-per; ENT-1860; ethene, tetrachloro-; ethylene tetrachloride; fedal-UN; NCI-C04580; NEMA; PER; perawin; PERC; perchloerethyleen, per; perchloroethylene; perclene; percloroetilene; percosolve; perk; perklore; persec; tetlen; teracap; tetrachlooretheen; tetrachloraethen; tetrachlorethylene; tetrachloroethene; tetrachloroethylene; 1,1,2,2-tetrachloroethylene; tetrachloroethylene (DOT); tetracloroefeen; tetraleno; tetralex; tetravec; tetrogner; tetropil.

Physical/Chemical Properties

Description: Colorless liquid; ether-like odor Boiling Point: 121°C Melting Point: -22.4°C Molecular Weight: 165.8 Chemical Formula: C1,C:CC1, Vapor Pressure: 15.8 mm at 22°C Vapor Density: 5.83 (air = 1) **Refractive Index:** $N_{D}^{25} = 1.5029$ Solubility: Miscible with alcohol, ether, and oils in all proportions; insoluble in water.

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Log Partition Coefficient (octanol/water): 2.88

Photochemical Reactivity: Photochemically reactive

Chemical Reactivity:

When heated to decomposition, emits toxic chloride fumes. Material is extremely stable and resists hydrolyzers. Reacts violently with Ba, Be, Li, N_2O_4 , and NaOH. May be handled in the presence or absence of air, water, and light with any of the common construction materials at a temperature up to 140°C.

Environmental Fate

The predominant fate of perchloroethylene is tropospheric photooxidation by hydroxyl radicals, which yields trichloroacetyl-chloride and phosgene. Rapid volatilization is the primary transport process. There is a moderate potential for bioaccumulation and possible biodegradation by higher organisms.

Source of Emissions

Production:

Made by chlorination of hydrocarbons, and pyrolysis of the carbon tetrachloride also formed. From acetylene and chloride via trichloroethylene.

Uses:

Dry cleaning solvent Manufacture of fluorocarbons Vapor-degreasing solvent Drying agent for metals and certain other solids Textile processing Vermifuge Heat transfer medium

Tables E-70 through E-74 present perchloroethylene production, consumption, and emission data.

Storage:

Store in a cool, dry, well-ventilated location, away from any area where the fire hazard may be acute.

Transportation:

Shipped in 5- and 55-gallon steel drums, tank cars, and tank trucks.

Location	Company ^a	Manufac- turing _b process	1978 capacity, 10 ⁶ kg	1978 estimated pro- duction, 10 ⁶ kg
California Pittsburg	Dow Chemical USA	C1-HC	20	10
Kansas Wichita	Vulcan Materials Co.	C1-HC	20	10
Kentucky Louisville	Stauffer Chemical Co.	C1-HC	30	20
Louisiana Baton Rouge Geismar Lake Charles Plaquemine	Ethyl Corporation Vulcan Materials Co. PPG Industries, Inc. Dow Chemical	C1-EDC C1-HC Ox-EDC C1-HC	20 70 90 50	10 40 50 30
Texas Corpus Christi Deer Park Freeport	DuPont ^C Diamond Shamrock Dow Chemical	C1-HC C1-EDC C1-EDC	70 75 70	40 40 40
Total			515	290

TABLE E-70. LOCATIONS OF AND PRODUCTION FIGURES FOR PERCHLOROETHYLENE FACILITIES

^aAn August 1978 article in <u>Chemical Marketing Reporter</u> stated that the Hooker Chemical Corporation facility at Taft, Louisiana stopped producing perc in March 1978.

^bKey to symbols: Cl-HC = Chlorination of C_1 to C_3 hydrocarbons or their partially chlorinated derivatives; Cl-EDC = chlorination of ethylene dichloride; Ox-EDC = oxychlorination of ethylene dichloride.

^CCaptive use only.

SRI International, 1979.

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Type of use	Consumption, 10 ⁶ kg	Percent of total
Dry cleaning	160	53
Metal cleaning	50	17
Chemical intermediate	40	13
Textile processing	20	7
Miscellaneous	30	10
Total	300	100

TABLE E-71. ESTIMATED CONSUMPTION OF PERCHLOROETHYLENE BY TYPE OF USE 1978

Source: SRI International, 1979.

TABLE	E-72.	ESTIMATED	NUMBEI	₹ OF	URBAN	DRY	CLEANERS	USING
	PER	CHLOROETHYL	ENE B	SI	ZE OF	OPER	ATION	

Turne	Number of operations			By numb of employ		
of operation	1 to 4	5 to 9	10 to 19	20 to 49	>50	Total
Commercial	4,200	1,900	850	700	120	7,770
Coin-operated	3,700	500	120	60	10	4,390
Industrial	20	10	20	100	110	260

Source: SRI International, 1979.

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	Fraction perchlore	n using Dethylene	Amount of perchloroethy used per plant, gal/yea		ethylene /year
	Number of	employees	N	lumber of employ	ees
Code ^a	0 to 20	>20	0 to 20	20 to 100	>100
331	0.00	0.11	-	1,800 ^a	10,000
336	0.00	0.06	-	45 ^a	250
339	0.00	0.14	-	12,000	67,200 ^a
342	0.00	0.09	-	2,655 ^a	14,752
343	0.00	0.14	-	2,750	15,400 ^a
344	0.00	0.08	-	350	1,960 ^a
345	0.00	0.18	-	863 ^a	4,795
347	0.08	0.11	330	5,262	17,044 ^a
349	0.00	0.14	-	1,310	7,336 ^a
352	0.00	0.11	-	90 ^a	500
361	0.00	0.07	-	149 ^a	825
362	0.17	0.00	219	-	-
364	0.00	0.07	-	73 ^a	403
366	0.00	0.11	-	176 ^a	980
367	0.06	0.00	700	-	-
371	0.00	0.05	-	110	616 ^a
372	0.10	0.22	10	490	25,703

TABLE E-73. ESTIMATED PERCHLOROETHYLENE USED FOR DEGREASING IN THE MANUFACTURING INDUSTRY

^aThese amounts have been extrapolated on the basis of the number of employees in the plant.

Source: SRI International, 1979.

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TABLE E-74. ESTIMATED EMISSIONS FROM PERCHLOROETHYLENE FACILITIES

location	Company	Estimated annual emissions 103 kg	Estimated emission rate g/s
		10 N3	3, 0
California Pittsburg	Dow Chemical USA	20	0.63
Kansas Wichita	Vulcan Materials Co.	20	0.63
Kentucky Louisville	Stauffer Chemical Co.	40	1.27
Louisiana Baton Rouge Geismar Lake Charles Plaquemine	Ethyl Corporation Vulcan Materials Co. PPG Industries, Inc. Dow Chemical	20 80 250 60	0.63 2.54 7.90 1.90
Texas Corpus Christi Deer Park Freeport	DuPont ^a Diamond Shamrock Dow Chemical	80 80 80	2.54 2.54 2.54

^aCaptive use for C_2 fluorocarbons; emission factor is unchanged.

Source: SRI International, 1979.

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Disposition:

Perchloroethylene may be disposed of by incineration, preferably after mixing with another combustible fuel. Care must be exercised to assure complete combustion to prevent the formation of phosgene. An acid scrubber is required to remove the halo acids produced. Alternatively, perchloroethylene may be recovered from waste gases and reused.

Sampling and Analytical Methods

- 1. NIOSH Method S335
 - a. Adsorption on charcoal.
 - b. Desorption with carbon disulfide.
 - c. Gas chromatography.
 - Detection limit: 136 to 4065 ng/m³ (20 to 600 ppm) for 3-liter sample

Possible interferences:

High humidity will lower vapor trapping efficiency. Any compound with the same retention time as perchloroethylene may be an interferent.

2. NIOSH Method P&CAM 127

- a. Adsorption on charcoal.
- b. Desorption with carbon disulfide.
- c. Gas chromatography.

Detection limit: 0.6 mg/m³ (0.01 ppm) with a 1-liter minimum sample size

Possible interferences: High humidity will lower vapor trapping efficiency. Any compound with the same retention time as perchloroethylene may be an interferent.

- 3. Method B (Appendix A): C_2-C_{18} hydrocarbons and other nonpolar organics with a boiling point 100° to 175°C.
 - a. Whole air collection in canister.
 - b. Cryogenic concentration.
 - c. Gas chromatography/flame ionization detection (gas chromatography/electron capture detection may also be used).
 - Detection limit:

0.1 ppb per 100-ml sample

Possible interferences: Storage time greater than a week is not recommended.

- 4. Method C (Appendix A): C_6-C_{12} hydrocarbons and other nonpolar organics with a boiling point between 60° and 200°C.
 - a. Adsorption on Tenax.
 - b. Thermal desorption.
 - c. Gas chromatography/mass spectrometry analysis (gas chromatography/electron capture detection may also be used).

Detection limit: 1 to 200 ppt for a 20-liter sample

Possible interferences: Blank levels usually limit sensitivity artifacts due to reactive components $(0_3, N0_x)$. Sample can be analyzed only once.

- 5. Method D (Appendix A): C_6-C_{12} hydrocarbons and other nonpolar organics with a boiling point of 60° to 200°C.
 - a. Adsorption on Tenax.
 - b. Thermal desorption into canisters.
 - c. Gas chromatography/flame ionization detection, or gas chromatography/mass spectrometry analysis (gas chromatography/electron capture detection may also be used).

Detection limit: 0.01 to 1 ppb for a 20-liter sample

Possible interferences: Blanks and artifact problems in Method C, above.

Permissible Exposure Limits

	OSHA	ACGIH
TWA STEL	100 ppm	50 ppm (335 mg/m ³) 200 ppm (1.340 mg/m ²)
Ceiling Peak	200 ppm 300 ppm (5 min. in 3 h)	

Human Toxicity

Acute Toxicity:

Moderate irritation effects via inhalation, oral, subcutaneous, intraperitoneal, and dermal routes. High toxicity via intravenous route. Not corrosive or dangerously acutely reactive, but toxic by inhalation, by prolonged or repeated contact with skin or mucous membrane, or when ingested by mouth. The liquid can cause injuries to the eyes. Exposures to higher than 200 ppm causes irritation, lachrymation, burning of the eyes, and irritation of the nose and throat. There may be vomiting, nausea, drowsiness, an attitude of

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irresponsibility, and even the appearance of alcholic intoxication. Also acts as an anesthetic. Can cause dermatitis, particularly after repeated or prolonged contact with skin, preceded by reddening and burning and more rarely, a blistering of the skin.

Chronic Toxicity:

Perchloroethylene caused hepatocellular carcinomas in mice of both sexes; however, a carcinogenesis bioassay was negative in rats. Therefore, perchloroethylene can be considered a suspected animal carcinogen.

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Chemical Name

Phenol

CAS Number

108-95-2

Chemical Classification

Phenol (aromatic alcohol)

Synonyms

Acide carbolique; Bakers P and S liquid and ointment; carbolic acid; carbolic acid (DOT); carbolsaure; fenol; fenolo; hydroxybenzene; monohydroxybenzene, NCI-50124; oxybenzene; phenic acid; phenole; phenyl hydrate; phenyl hydroxide; phenylic acid; phenylic alcohol.

Physical/Chemical Properties

Description: White crystalline mass that turns pink or red if not perfectly pure or if under influence of light; absorbs water from the air and liquifies; distinctive odor; sharp burning taste. When in very weak solution, has a sweetish taste. Boiling Point: 182°C Melting Point: 42.5° to 43°C Molecular Weight: 94.1 Chemical Formula: C_6H_5OH Vapor Pressure: 1 mm at 40.1°C Vapor Density: 3.24 (air = 1) **Refractive Index:** $N_0^{41} = 1.5408$

Solubility: Soluble in alcohol, water, ether, chloroform, glycerol, carbon disulfide, petrolatum, fixator volatile oils or alkalines. Log Partition Coefficient (octanol/water): 1.46 Photochemical Reactivity: Reactivity toward OH· is 2 times butane. Reactivity toward 0₃ is a 9.6-hour half-life or 15 percent of propylene. Chemical Reactivity: Reacts violently with (AlCl₃ + nitrobenzene), butadiene, peroxydisulfuric acid, and peroxymonosulfuric acid. Moderate fire hazard when exposed to heat, flame, or oxidizers. When heated, emits toxic fumes, can react with oxidizing materials.

Environmental Fate

Photooxidation of volatilized phenol and photolysis of phenolic anion may both take place at moderate rates. Metal catalyzed oxidation may take place in highly aerated waters. No bioaccumulation, but extensive biodegradation in natural waters.

Source of Emissions

Production: Oxidation of cumene Derivation from benzoic acid

Uses:

Phenolic resins Epoxy resins (bisphenol-A) Nylon 6 (caprolactam) 2.4-D Selective solvent for refining lubricating oils Adipic acid Salicylic acid Phenolphthaline Pentachlorophenol Acetophenetidine Picric acid Germicidal paints Pharmaceuticals Laboratory reagent Dyes and indicators Slimicide General disinfectant

Tables E-75 through E-83 and Figure E-5 present phenol production, consumption, and emission data.

Company	Location	1978 capacity, ^a 10 ⁶ lb/yr	1978 production, ^a 10 ⁶ lb/yr	Geographical location, latitude/longitude
Ferro Corporation	Sante Fe Springs, CA	12	5.4	33 56 30/118 04 18
Koppers	Follansbee, WV	12	5.4	40 23 10/80 35 07
Merichem	Houston, TX	12	5.4	29 45 36/95 10 48
Stimson Lumber	Anacortes, WA	12	5.4	48 28 31/122 32 48
U.S. Steel Corporation	Clairton, PA	12	5.4	40 18 15/79 52 43
Total		60	27	

TABLE E-75. PHENOL PRODUCERS (NATURAL PHENOL)

^a Total capacity and production distributed evenly over all five sites in the absence of capacity figures. Source: Systems Applications, Inc. 1980.

Company	Location	1978 capacity, 10 ⁶ lb/yr	1978 production, ^a 10 ⁶ lb/yr	Geographical location, latitude/longitude
Allied Chemical	Philadelphia, PA	600	453	40 00 24/75 04 07
Clark	Blue Island, IL	88	66	41 39 21/87 41 56
Dow	Freeport, TX	465	351	28 59 12/95 24 05
Georgia Pacific	Plaquemine, LA	265	200	30 15 00/91 11 00
Getty	El Dorado, KS	95	72	37 47 10/96 52 00
Kalama	Kalama, WA	75	57	46 00 54/122 51 05
Monsanto	Chocolate Bayou, TX	500	377	20 14 55/95 12 45
Shell	Deer Park, TX	500	377	29 42 57/95 07 28
Standard Oil of California	Richmond, CA	55	42	37 56 12/122 20 48
Union Carbide	Bound Brook, NJ	180	135	40 33 32/74 31 18
U.S. Steel	Haverhill, OH	325	245	38 34 52/82 49 36
Total		3148	2375	

TABLE E-76. PHENOL PRODUCERS (SYNTHETIC PHENOL)

^a Total production distributed based on individual site capacity.

Source: Systems Applications, Inc. 1982.

TABLE E-77. PHENOL END-USE 1978 (SYNTHETIC AND NATURAL PHENOL)

Source	Usage, 10 ⁶ 1b/yr	Percent usage
Phenolic resins Bisphenol-A Caprolactam Nonylphenol Salicylic acid Dodecylphenol Adipic acid Miscellaneous Exports	1045 405 355 48 48 24 24 24 382 71	44 17 15 2 2 1 1 15 3
Total	2402	100

Source: Systems Applications, Inc. 1980.

Source	Nationwide emissions, lb/yr
Production	3,708,080
Phenolic resins	522,500
Bisphenol-A	202,500
Caprolactam ^a	511,200
Nonylphenol	41,700
Salicylic acid	24,000
Dodecylphenol	- 24,000
Miscellaneous	259,760
Export	0
Total	5,293,740

TABLE E-78. 1978 PHENOL NATIONWIDE EMISSIONS

^a Includes emissions from adipic acid manufacture.

Source: Systems Applications, Inc. 1982.

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Company	Location	1978 capacity, 10 ⁶ lb/yr	1978 production, 10 ⁶ lb/yr	Geographical location, latitude/longitude
CompanyLocationBisphNowGeneral ElectricStellJ.S. SteelJ.S. SteelTotalTotalCaproAlliedHopewell, VATotalSorg WarnerKAFKalamaKohm and HaasSchenectadySchenectady	Bisphenol-	A producers		
Dow General Electric Shell U.S. Steel	Freeport, TX Mount Vernon, IN Deer Park, TX Haverhill, OH	150 220 150 <u>120</u>	95 140 95 <u>75</u>	28 59 12/95 24 05 37 56 42/87 34 25 29 42 55/95 07 34 38 34 52/82 49 36
	Total	640	405	
	Caprolacta	m producer		
Allied	Hopewell, VA	<u>400</u>	<u>355</u>	37 22 13/77 18 08
	Total	400	355	
	Nonylpheno	1 producers		
Borg Warner Exxon GAF Jefferson Kalama Monsanto Rohm and Haas Schenectady	Morgantown, WV Bayway, NJ Calvert City, KY Linden, NJ Port Neches, TX Kalama, WA Kearney, NJ Deer Park, TX Philadelphia, PA Rotterdam Junction, NY Oyster Creek, TX	60 20 5 20 35 20 40 10 20 20 50	10 3 1 3 6 3 6 2 3 3 8	39 40 39/80 58 34 40 38 46/74 11 48 37 02 50/88 21 12 40 38 19/74 15 26 29 57 45/93 56 00 46 00 54/122 51 05 40 46 12/74 09 08 29 43 30/95 06 15 39 54 50/75 11 30 42 47 22/73 43 12 29 58 21/95 20 38
	Total	300	48	

TABLE E-79. PHENOL USER LOCATIONS

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TABLE E-79 (continued)

Company	Location	1978 capacity, 10 ⁶ lb/yr	1978 production, 10 ⁶ lb/yr	Geographical location, latitude/longitude
	Salicylic a	acid producers		
Dow Monsanto Sterling Drug Tenneco	Midland, MI St. Louis, MO Cincinnati, OH Garfield, NJ	15 20 8 10	14 18 7 9	43 35 28/84 13 08 38 34 37/90 11 42 39 05 15/84 33 09 40 52 28/74 06 49
	Total	53	48	
	Dodecylphe	enol producers	······································	
Borg Warner GAF Monsanto	Morgantown, WV Calvert City, KY Kearney, NJ	60 5 40	4 1 9	39 40 39/80 58 34 37 02 05/88 21 12 40 46 12/74 09 08
	Total	105	14	
	Adipic ac	id producer		
Allied	Hopewell, VA	30	24	37 22 13/77 18 08
	Total	30	24	

Source: Systems Applications, Inc. 1980.

		Process	Storage	Fugitive	Total em	nissions
Company	Location	lb/yr	lb/yr	lb/yr	lb/yr	g/s
Allied	Philadelphia, PA	23,000	172,000	12,740	207,740	2.99
Clark	Blue Island, IL	117,480	1,980	27,060	146,520	2.11
Dow	Freeport, TX	624,780	10,530	143,910	779,220	11.22
Georgia Pacific	Plaquemine, LA	356,000	6,000	82,000	444,000	6.39
Getty	El Dorado, KS	128,160	2,160	29,520	159,840	2.30
Kalama	Kalama, WA	101,460	1,710	23,370	126,540	1.82
Monsanto	Chocolate Bayou, TX	8,419	142	1,939	10,500	.15
Shell	Deer Park, TX	671,060	11,310	154,570	836,940	12.05
Standard Oil of California	Richmond, CA	74,760	1,260	17,220	93,240	1.34
Union Carbide	Bound Brook, NJ	240,300	4,050	55,350	299,700	4.31
U.S. Steel	Haverhill, OH	436,100	7,350	100,450	543,900	7.83
Ferro	Sante Fe Springs, CA	9,612	162	2,214	11,988	0.17
Koppers -	Follansbee, WV	9,612	162	2,214	11,988	0.17
Merichem	Houston, TX	9,612	162	2,214	11,988	0.17
Stimson	Anacortes, WA	9,612	162	2,214	11,988	0.17
U.S. Steel	Clairton, PA	9,612	162	2,214	11,988	0.17
Total		2,829,579	219,302	659,199	3,708,080	

TABLE E-80. PHENOL EMISSIONS FROM PHENOL PRODUCERS

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Source: Systems Applications, Inc. 1982.

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<u></u>	Emission factor, 1b phenol lost per 1b used (produced)							
Source	Process	Storage	Fugitive	Total	Derivation ^a			
Phenol production	0.00178	0.00003	0.00041	0.00222	С			
Caprolactam	0.00130	0.00001	0.00013	0.00144	A			
Bisphenol-A	0.00035	0.00003	0.00012	0.00050	С			
Nonylphenol	0.00080	0.00001	0.00019	0.00100	С			
Salicylic acid	0.00035	0.00001	0.00014	0.00050	С			
Dodecylphenol	0.00080	0.00001	0.00019	0.00100	D			
Phenolic resins	0.00035	0.00002	0.00013	0.00050	D			
Adipic acid	Phenol er duction	nissions ar losses	e included	with cap	rolactam pro-			
Miscellaneous				0.00068 ^b				

TABLE E-81. PHENOL PRODUCTION AND END-USE EMISSION FACTORS

^a A - Site visit data, B - State files, C - Published data, D - Hydroscience estimate

^b Based on a weighted average of all other phenol end-use emission factors.

Source: Systems Applications, Inc. 1980.

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		Phenol emissions						
		Process	Storage	Fugitive	Total			
Company	Location	lb/yr	lb/yr	lb/yr	lb/yr	g/s		
	•	Bisphenol-A	producers					
Dow	Freeport, TX	33,250	2,850	11,400	47,500	0.68		
General Electric	Mount Vernon, IN	49,000	4,200	16,800	70,000	1.01		
Shell	Deer Park, TX	33,250	2,850	11,400	47,500	0.68		
U.S. Steel	Haverhill, OH	26,250	2,250	9,000	37,500	0.54		
	Total	141,750	12,150	48,600	202,500			

TABLE E-82. PHENOL EMISSIONS FROM END USERS

		Caprolactam	producer			
Allied	Hopewell, VA	461,500	3,550	46,150	511,200	7.36
		Nony1pheno1	producers	· · · · · · · · · · · · · · · · · · ·	I	
Borg Warner	Morgantown, WV	8,000	100	1,900	10,000	0.144
Exxon	Bayway, NJ	450	28	522	1,000	0.014.
GAF	Calvert City, KY	800	10	190	1,000	0.014
	Linden, NJ	2,400	30	570	3,000	0.043
Jefferson	Port Neches, TX	4,800	60	1,140	6,000	0.086
Kalama	Kalama, WA	2,400	30	570	3,000	0.043
Monsanto	Kearny, NJ	1,360	17	323	1,700	0.024
Rohm and Haas	Deer Park, TX	1,600	20	380	2,000	0.029
	Philadelphia, PA	2,400	30	570	3,000	0.043

(continued)

TABLE E-82 (continued)

ka na manana na mana	Phenol emissions					
		Process	Storage	Fugitive	Tot	al
Company	Location	1b/yr	lb/yr	lb/yr	lb/yr	g/s
	Nony	lphenol produ	cers (continued)		
Schenectady	Rotterdam Junction, NY	2,400	30	570	3,000	0.043
	Oyster Creek, TX	6,400	80	1,520	8,000	0.115
	Total	33,010	435	8,255	41,700	
	-	Salicylic aci	d producers			
Dow	Midland, MI	4,900	140	1,960	7,000	0.101
Monsanto	St. Louis, MO	6,300	180	2,520	9,000	0.130
Sterling Drug	Cincinnati, OH	2,450	70	980	3,500	0.050
Tenneco	Garfield, NJ	3,150	3,150 90 1,260		4,500	0.065
	Total	16,800	480	6,720	24,000	
	•	Dodecylphend	ol producers			
Borg Warner	Morgantown, WV	11,200	140	2,660	14,000	0.202
GAF	Clavert City, KY	800	10	190	1,000	0.014
Monsanto Kearny, NJ		7,200	90	1,710	9,000	0.130
	Total	19,200	240	4,560	24,000	
		Adipic acio	l producer			
Allied	Hopewell, VA	Emissior	is are included	in caprolactam p	production	osses

Source: Systems Applications, Inc. 1982.

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					Stan	Plant	Source	Emi	Emissions, g/s	
No.	Company	Site	Latitude	Longitude	station	type ^a	type ^b	Process	Storage	Fugitive
1	Allied	Frankford, PA	40 18 15	079 52 43	14762	1	1	11.611296	0.195696	2.674512
2	Clark	Blue Island, IL	41 39 21	087 41 56	14855	1	1	1.691712	0.028512	0.389664
3	Georgia Pacific	Plaquemine, LA	30 15 00	091 11 00	13970	1	1	5.126400	0.086400	1.180800
4	Getty	El Dorado, KS	37 47 10	096 52 00	03920	1	1	1.845504	0.031104	0.425088
5	Monsanto	Chocolate Bayou, TX	29 14 55	095 12 45	12906	1	1	9.663264	0.162864	2.225808
6	Standard	Richmond, CA	37 56 12	122 20 48	12906	1	1	1.076544	0.018144	0.247968
7	Union Car- bide	Bound Brook, NJ	40 33 32	074 31 18	94741	1	1	3.468320	0.058320	0.797040
8	Ferro	Sante Fe Springs, CA	33 56 30	118 04 18	93106	1	1	0.138413	0.002338	0.031882
9	Koppers	Follansbee, WV	40 23 10	080 35 07	14762	1	1	0.138413	0.002338	0.031882
10	Merichem	Houston, TX	29 45 36	095 10 48	12906	1	1	0.138413	0.002338	0.031882
11	Stimson	Anacortes, WA	48 28 31	122 32 48	24217	1	1	0.138413	0.002338	0.031882
12	U.S. Steel	Clairton, PA	40 18 15	079 52 43	14762	1	1	0.138413	0.002338	0.031882
13	Dow	Freeport, TX	28 59 30	095 23 35	12923	2	1 2	8.996832 0.478800	0.151632 0.041040	2.072304 0.164160
14	Shell	Deer Park, TX	29 43 30	095 06 15	12986	2	1 2	9.663264 0.478800	0.162864 0.041040	2.225888 0.164160
15	U.S. Steel	Haverhill, OH	38 34 53	083 49 36	13866	2	1	6.279840 0.378000	0.105840 0.032400	1.446480 0.129600

TABLE E-83. EMISSIONS AND METEOROLOGICAL STATIONS OF SPECIFIC POINT SOURCES OF PHENOL

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TABLE E-83 (continued)

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		· · · · · · · · · · · · · · · · · · ·			Star	Plant	Source	Emi	ssions, g/	s
No.	Company	Site	Latitude	Longitude	station	type ^a	type ^b	Process	Storage	Fugitive
16	Kalama	Kalama, WA	46 00 54	122 51 05	24229	3	1 4	1.461024 0.034560	0.024624 0.000432	0.836528 0.008208
17	General Electric	Mount Vernon, IN	37 56 43	087 34 25	93817	4	3	0.705600	0.060480	0.241920
18	Allied	Hopewell, VA	37 23 13	077 18 08	13740	5	3	6.643600	0.051120	0.664560
19	Exxon	Bayway, NJ	40 38 46	074 11 48	94741	6	4	0.034560	0.000432	0.008208
20	GAF	Linden, NJ	40 38 19	074 15 26	94741	6	4	0.034560	0.000432	0.008208
21	Jefferson	Port Neches, TX	29 57 45	093 56 00	12917	6	4	0.069120	0.000864	0.016416
22	Rohm and	Deer Park, TX	29 43 00	095 06 15	12906	6	4	0.028040	0.000288	0.005472
	Haas									
23	Rohm and Haas	Philadelphia, PA	39 54 50	075 11 30	13739	6	4	0.034560	0.000432	0.008208
24	Schenectady	R Junction, NY	42 47 22	073 43 12	14735	6	4	0.034560	0.000432	0.008208
25	Schenectady	Oyster Creek, TX	29 58 21	095 20 38	12960	6	4	0.092160	0.001152	0.021888
26	Borg Warner	Morgantown, PA	39 40 39	080 58 34	13736	7	4 6	0.115200 0.161288	0.001440 0.002016	0.027360 0.038304
27	GAF	Calvert City, KY	37 02 50	088 21 12	03816	7	4 6	0.011520 0.011520	0.000144 0.000144	0.002736 0.002736
28	Monsanto	Kearny, NJ	40 46 12	074 09 08	94741	7	4 6	0.069120 0.103680	0.000864 0.001296	0.016416 0.024624
29	Dow	Midland, MI	43 35 28	084 13 08	14845	8	5	0.070560	0.002016	0.028224
30	Monsanto	St. Louis, MO	33 34 37	097 11 42	13994	8	5	0.090720	0.002592	0.036288
31	Sterling	Cincinnati, OH	39 05 15	084 33 09	13840	8	5	0.035280	0.001008	0.014112
32	Tenneco	Garfield, NJ	40 52 28	074 06 47	94741	8	5	0.045360	0.001296	0.018144

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TABLE E-83 (continued)

- ^a Plant types: 1 plant produces phenol; 2 plant produces phenol and Bisphenol-A; 3 plant produces phenol and nonylphenol; 4 plant produces Bisphenol-A; 5 plant produces caprolactam and adipic acid; 6 plant produces nonylphenol; 7 plant produces nonylphenol and dodecylphenol; 8 plant produces salicylic acid.
- ^b Source types: 1 phenol production; 2 Bisphenol-A production; 3 caprolactam/adipic acid production; 4 - nonylphenol production; 5 - salicylic acid production; 6 - dodecylphenol production.

Source: Systems Applications, Inc. 1982.



NOTE: NUMERALS DENOTE NUMBER OF PLANTS.

Figure E-5. Specific point sources of phenol emissions.

Source: Systems Applications, Inc. 1980.

Storage:

Should be protected from physical damage, and stored in a cool, dry, well-ventilated location, away from any areas where the fire hazard may be acute. Outside or detached storage is preferred, separate from other storage. Spills must be disposed of immediately by properly protected personnel.

Transportation:

Should be shipped in bottles, cans, drums, tankcars, tank barges. Must be labled "Poison B."

Disposition: Phenol may be disposed of by incineration.

Sampling and Analytical Methods

- 1. NIOSH Method S330
 - a. Bubbler (0.1 <u>N</u> sodium hydroxide).
 - b. Gas chromatography.
 - c. Flame ionization detector.

Detection limit: 0.25 ppm with 100-liter sample

Possible interferences: None identified.

2. Method C (Appendix A): C_6-C_{12} hydrocarbons and other nonpolar organics with boiling point between 60° and 200°C.

- a. Adsorption on Tenax.
- b. Thermal desorption.
- c. Gas chromatography/mass spectrometry analysis.

Detection limit: 1 to 200 ppt for a 20-liter sample

Possible interferences: Blank levels usually limit sensitivity artifacts due to reactive components (O_3, NO_x) . Sample can be analyzed only once.

3. Method S

Permissible Exposure Limits

OSHA (skin)ACGIH (skin)NIOSHTWA5 ppm (19 mg/m³)5 ppm (19 mg/m³)20 mg/m³STEL10 ppm (38 mg/m³)60 mg/m³ (15 min)

Odor Perception: 0.022 mg/m³

Human Toxicity

Acute Toxicity:

Phenol vapor or liquid is readily absorbed through the skin or any mucous membrane, which may cause acute and chronic poisoning. A concentrated solution causes bad acid burns. Phenol is not sufficiently volatile to constitute a respiratory hazard under normal conditions. High toxicity for oral, intraperitoneal, subcutaneous, and parenteral methods. Moderate irritant to skin, subcutaneous, oral, and parenteral area. In acute poisoning, mainly effects central nervous system. Absorption from spilling phenolic solutions on skin may be very rapid, and death results from colapse within 30 minutes to several hours. Death has resulted from phenol absorption through 64 in.² of skin area. Where death is delayed, damage to kidneys, liver, pancreas, and spleen; and edema of the lungs may result. Dermatitis resulting from contact with phenol or phenol-containing product is fairly common. As little as 1.5 g (oral) has killed.

Chronic Toxicity:

Phenol as a nonspecific irritant may promote development of tumors when applied repeatedly to the skin in large amounts. Results were negative in a carcinogenesis bioassay completed by the National Cancer Institute.

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Chemical Name

Phosgene

CAS Number

75-44-5

Chemical Classification

Chlorinated carbonyl

Synonyms

Carbone (oxychlorure de); carbon oxychloride; carbonylchlorid; carbonyl chloride; CG; chloroformyl chloride; carbino (ossichoruro di) diphosgene; fosgeen; fosgen; fosgene; koolstofoxychloride; NCI-60219; phosgen; phosgene (DOT)

Physical/Chemical Properties

Description: Liquid or easily liquified gas; colorless to light yellow; odor varies from strong to stifling when concentrated to hay-like or diluted form. Boiling Point: 8.2°C Melting Point: -128°C Molecular weight: 98.9 Chemical Formula: COC1, Vapor Pressure: 1180 mm at 20°C Vapor Density: 3.4 (air = 1)Refractive Index: Not available Solubility: Slightly soluble in water and slowly hydrolized. Soluble in benzene and toluene. Log Partition Coefficient (octanol/water): Not available

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Photochemical Reactivity:

In the atmosphere, phosgene decomposes in water to form hydrochloric acid.

Chemical Reactivity:

Decomposes in water to form hydrochloric acid. Because of its high degree of reactivity, phosgene interacts with many classes of inorganic and organic reagents. Reacts violently with Al, tert-butyl azido formate, 2,4-hexadiyn-1,6-diol, isopropyl alcohol, K, Na, hexafluoro isopropylidene, amino lithium, lithium.

Environmental Fate

Rapid hydrolysis to CO_2 and HCl is the principal fate. Photolysis can occur, but cannot compete with hydrolysis.

Source of Emissions

Production:

Obtained by passing a mixture of carbon monoxide and chlorine over activated carbon.

Uses:

Organic synthesis, especially in isocyanates, polyurethane and polycarbonate resins, carbonates, organic carbonates, and chloroformates. Pesticides Herbicides Dye manufacture

Tables E-84 through E-92 and Figure E-6 graphically present phosgene production, consumption, and emission data.

Storage:

Should be protected against physical damage and stored outdoors or in a well-ventilated area of noncombustible construction.

Transportation:

Should be shipped in steel cylinders and tank cars. All phosgene containers require "Poison A" labels.

Disposition:

Because of its low boiling point and high toxicity, phosgene should never be allowed to enter drains or sewers. If recycling of phosgene is not feasible, phosgene waste can be handled by caustic scrubbing in packed columns.

Sampling and Analytical Methods

- 1. NIOSH Method 219
 - a. Midget impinger.
 - b. Nitrobenzylpyridine.

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c. Calorimetric analysis.

Company	Location	1978 capacity, 10 ⁶ lb/yr	1978 production, 10 ⁶ lb/yr	Geographical location, latitude/longitude
Allied Chemical	Moundsville, WV	100	76	39 54 24/80 47 51
BASF Wyandotte	Geismar, LA	55	41.8	30 11 34/91 00 42
Chemtron	LaPorte, TX	80	60.8	29 39 20/95 02 18
Dow Chemical	Freeport, TX	130	98.8	28 59 12/95 24 05
DuPont	Deepwater, NJ	135	102.6	39 41 25/75 30 35
General Electric	Mt. Vernon, IN	60	45.6	37 56 42/87 54 25
Jefferson	Port Neches, TX	30	22.8	30 18 50/95 23 06
Minerec	Baltimore, MD	8	6.1	39 14 11/76 34 41
Mobay Chemical	Baytown, TX	250	190	29 45 30/94 54 25
•	New Martinsville, WV	250	190	39 43 35/80 49 43
Olin	Ashtabula, OH	50	38	41 53 46/80 43 22
	Lake Charles, LA	120	91.2	30 13 55/93 15 57
PPG	Barberton, OH	5	3.8	41 00 37/81 36 29
Rubicon Chemicals	Geismar, LA	130	98.8	30 12 00/91 00 30
Stauffer Chemicals	Cold Creek, AL	25	19	30 58 30/88 01 16
Upjohn	LaPorte, TX	200	152	29 42 26/95 04 29
Van De Mark	Lockport, NY	8	6.1	43 11 08/78 42 40
Total		1,636	1,243.4	

TABLE E-84. PHOSGENE PRODUCERS

Source: Systems Applications, Inc. 1982.

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	TABLE	E-85.	PHOSGENE	END-USE	DISTRIBUTION
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Source	Usage, 10 ⁶ lb/yr	Percent usage		
Toluene diisocyanates (TDI) Polymeric isocyanates (MDI) Polycarbonates Miscellaneous	814.5 339.5 67.8 135.6	60 25 5 10		
Total	1357.4	100		

Source: Systems Applications, Inc. 1980.

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Company	Location	1978 MDI capacity, 10 ⁶ lb/yr	1978 phosgene use, 10 ⁶ 1b/yr	Geographical location, latitude/longitude			
Mobay Chemical	Baytown, TX New Martinsville, WV	110 50	81.25 36.9	29 45 30/94 54 25 39 44 50/80 50 50			
Rubicon Chemicals	Geismar, LA	50	36.9	30 12 00/91 00 30			
Upjohn	LaPorte, TX	250	184.4	29 42 26/95 04 29			
Total		460	339.5				

TABLE E-86. PHOSGENE USERS (manufacturers of polymeric isocyanates)

Source: Systems Applications, Inc. 1980.

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Company	Location	1978 TDI capacity, 10 ⁶ 1b/yr	1978 phosgene use, 10 ⁶ lb/yr	Geographical location, latitude/longitude
Allied Chemical	Moundsville, WV	80	80.9	39 54 39/80 44 49
BASF Wyandotte	Geismar, LA	100	101.2	30 11 34/91 00 42
Dow Chemical	Freeport, TX	100	101.2	28 59 12/95 24 05
DuPont	Deepwater, NJ	70	70.8	39 41 25/75 30 35
Mobay Chemical	Baytown, TX	130	131.5	29 45 30/94 54 25
	New Martinsville, WV	100	101.2	39 44 50/80 50 50
Olin	Ashtabula, OH	30	30.4	41 53 07/80 45 50
	Lake Charles, LA	100	101.2	30 13 55/93 15 57
Rubicon Chemicals	Geismar, LA	40	40.5	30 12 00/91 11 30
Total	750	758.9		

TABLE E-87. PHOSGENE USERS [manufacturers of toluene diisocyanate (TDI)]

Source: Systems Applications, Inc. 1982.

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		Phosgene	emissions
Company	Location	lb/yr	g/s
Allied Chemical	Moundsville, WV	14,214	0.204
BASF Wyandotte	Geismar, LA	8,190	0.118
Chemtron	LaPorte, TX	10,964	0.158
Dow Chemical	Freeport, TX	18,450	0.264
DuPont	Deepwater, NJ	18,934	0.273
General Electric	Mt. Vernon, IN	8,208	0.118
Jefferson	Port Neches, TX	4,104	0.059
Minerec	Baltimore, MD	1,098	0.016
Mobay Chemical	Baytown, TX New Martinsville, WV	35,548 35,086	0.511 0.505
Olin	Ashtabula, OH Lake Charles, LA	7,020 17,082	0.101 0.246
PPG	Barberton, OH	684	0.01
Rubicon Chemicals	Geismar, LA	18,270	0.263
Stauffer Chemicals	Cold Creek, AL	3,420	0.049
Union Carbide	S. Charleston, WV	20,086	0.30
Upjohn	LaPorte, TX	28,580	0.412
Van De Mark	Lockport, NY	1,098	0.016
Total		251,036	3,624

TABLE E-88. TOTAL PHOSGENE EMISSIONS FROM PRODUCERS AND USERS

Source: Systems Applications, Inc. 1982.

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	Production/usage.		Total emissions		
Source	10 ⁶ 1b/h	Percent usage	lb/yr	g/s	
Producers	1357.4	-	190,960	2.749	
Users:					
Toluene diisocyanate	746.0	60	4,998	0.078	
Polymeric isocyanates	310.9	25	2,140	0.031	
Polycarbonates	62.2	5	447 ^a	0.006	
Miscellaneous	124.3	10	893 ^a	0.012	
Total	2600.8	100	199,438	2.876	

TABLE E-89. SOURCES OF PHOSGENE EMISSIONS

^a Based on emission factor for toluene diisocyanate (TDI)

Source: Systems Applications, Inc. 1982.

TABLE E-90. PHOSGENE EMISSIONS FROM PHOSGENE USERS FOR MDI PRODUCTION

		Process vent emissions		Fugitive emissions		Total emissions	
Company	Location	lb/yr	g/s	lb/yr	g/s	lb/yr	g/s
Mobay Chemical	Baytown, TX	480	0.007	Nil	Nil	480	0.007
	New Martinsville, WV	220	0.003	Nil	Nil	220	0.003
Rubicon Chemicals	Geismar, LA	220	0.003	Nil	Nil	220	0.003
Upjohn	LaPorte, TX	1220	0.018	Nil	Nil	1220	0.018
Total		·······				2140	0.031

Source: Systems Applications, Inc. 1980.

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		Process vent emissions		Fugitive emissions		Total emissions	
Company	Location	1b/yr	g/s	lb/yr	g/s	lb/yr	g/s
Allied Chemical	Moundsville, WV	534	0.008	Ni1	Nil	534	0.008
BASF Wyandotte	Geismar, LA	666	0.01	Nil	Ni]	666	0.01
Dow Chemical	Freeport, TX	666	0.01	Ni]	Nil	666	0.01
DuPont	Deepwater, NJ	466	0.007	Nil	Nil	466	0.007
Mobay Chemical	Baytown, TX	868	0.012	Nil	Nil	868	0.012
	New Martinsville, WV	666	0.01	Nil	Nil	666	0.01
Olin	Ashtabula, OH	200	0.003	Nil	Nil	200	0.003
	Lake Charles, LA	666	0.01	Nil	Nil	6 66	0.01
Rubicon Chemicals	Geismar, LA	266	0.004	Nil	Nil	266	0.004
Total						4,998	0.074

TABLE E-91. PHOSGENE EMISSIONS FROM PHOSGENE USERS FOR IDI PR	RUDUCTION
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Source: Systems Applications, Inc. 1982.

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					Star	Plant	Source	Emi	ssions, g	/s
No.	Company	Site	Latitude	Longitude	station	type ^a	type ^b	Process	Storage	Fugitive
1	Allied Chemical	Moundsville, WV	39 54 39	080 44 49	13736	1	1	0.002442	0.	0.062437
2	BASF Wyan- dotte	Ceismar, LA	30 11 34	091 00 42	13979	1	1	0.000349	0.	0.003964
3	Dow	Freeport, TX	28 59 30	095 23 35	12923	1	1	0.256089	0.	0.009576
4	DuPont	Deepwater, NJ	39 41 25	075 30 35	13739	1	1	0.006722	0.	0.265950
5	Mobay	Baytown, TX	29 45 30	094 54 25	12906	1	1	0.019502	0.	0.492485
6	Mobay	New Martins- ville, WV	39 44 50	080 50 50	13736	1	1	0.492485	0.	0.012748
7	01in	Astabula, OH	41 53 07	080 45 50	14843	1	1	0.002886	0.	0.098491
8	Olin	Lake Charles, LA	30 13 55	093 15 57	03937	1	1	0.000095	0.	0.002220
9	Rubicon	Geismar, LA	30 12 00	091 11 30	12958	1	1	0.007008	0.	0.256088
10	Upjohn	LaPorte, TX	29 42 36	095 04 29	12906	1	1	0.017567	0.	0.393994
11	Chemetron	LaPorte, TX	29 39 20	095 02 18	12906	2	1	0.	0.	0.151890
12	General Electric	Mt. Vernon, IN	37 56 42	087 34 25	93817	2	1	0.	0.	0.118182
13	Jefferson	Port Neches, TX	29 57 45	093 56 00	12917	2	1	0.	0.	0.059107
14	Minerec	Baltimore, MD	39 14 11	076 34 41	13701	2	1	0.	0.	0.015823
15	ITC	Barberton, OH	41 00 37	081 36 29	14095	2	1	0.	0.	0.009323
16	Stauffer	Cold Creek, AL	30 58 30	088 01 16	93841	2	1	0.	0.	0.049245
17	Vandermark	Lockport, NY	43 11 08	078 42 40	14747	2	1	0.	0.	0.015823

TABLE E-92. EMISSIONS AND METEOROLOGICAL STATIONS OF SPECIFIC POINT SOURCES OF PHOSGENE

^a Plant types: 1 - plant produces and consumes phosgene; 2 - plant produces phosgene.

^b Source types: 1 - phosgene production/consumption processes.

Source: Systems Applications, Inc. 1980.



NOTE: NUMERALS DENOTE NUMBER OF PLANTS.

Figure E-6. Specific point sources of phosgene emissions.

Source: Systems Applications, Inc. 1980.

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Detection limit: 0.005 ppm with a 250-liter sample

Possible interferences: Other acid chlorides, alkyl and aryl derivatives that are substituted by active halogen atoms, and sulfate esters are known to produce color with this reagent.

Because this compound is highly unstable, a field determination should be made. A manual colorimetric test using 4-nitrobenzylpyridine appears to be the best approach for routine analysis (detection limit approximately 0.05 ppm for 25-liter sample).

Permissible Exposure Limits

	OSHA	ACGIH	NIOSH
TWA Ceiling	0.1 ppm (0.4 mg/m ³)	0.1 ppm (0.4 mg/m ³)	0.1 ppm 0.2 ppm

Odor Perception 0.5 to 1 ppm.

Human Toxicity

Acute Toxicity:

High toxicity via inhalation. High irritant to eyes and mucous membrane at 4 ppm. In presence of moisture, phosgene decomposes to form hydrochloric acid and carbon monoxide. This action takes place within the body when the gas reaches the bronchioles and the alevoli of the lungs. There is little irritation effect upon the respiratory tract; therefore, the warning properties of the gas are very slight. Concentrations of 3 to 5 ppm of phosgene in air cause irritation of the eyes and throat, with coughing; 25 ppm is dangerous for exposure lasting 30 to 60 minutes; and 50 ppm is rapidly fatal even after short exposure.

Chronic Toxicity:

Epidemiologic studies have shown no ill effects definitely attributable to phosgene in 326 workers exposed to an average of 0.125 ppm or less for considerable periods.

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a.

Chemical Name

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Propylene oxide

CAS Number

75-56-9

Chemical Classification

Epoxide

Synonyms

Epoxypropane; 1,2-epoxypropane; ethylene oxide, methyl; methyl ethylene oxide; methyl oxirane; NCI-50099; oxirane, methyl; oxyde de propylene; propane, epoxy-; propene oxide; propylene oxide; 1,2-propylene oxide; propylene oxide (DOT).

Physical/Chemical Properties

Description: Colorless liquid; ethereal odor. Boiling Point: 33.9°C Melting Point: -104.4°C Molecular Weight: 58.8 Chemical Formula: CH2-CH-CH3 Vapor Pressure: 445 mm (20°C) 400 mm at 17.8°C Vapor Density: 2.0 (air = 1)Refractive Index: $N_{D}^{20} = 1.3670$ Solubility: Partially soluble in water, soluble in alcohol and ether. Log Partition Coefficient (octanol/water): Not available

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Photochemical Reactivity: Not available

Chemical Reactivity:

Reacts with active hydrogen compounds (e.g., alcohols, amines) and with inorganic chloride in foods to form 1-chloro-2propanol. Also reacts with 4-(4'-nitrobenzyl)pyridine. Violent reaction with NH₄OH, chlorosulfonic acid, HCl, HF, HNO₃, oleum, and H₂SO₄.

Environmental Fate

Propylene oxide exhibits a high degree of reactivity with a large number of chemicals including water.

Source of Emissions

Production:

Chlorohydration of propylene, followed by saponification with lime.

Peroxidation of propylene.

Epoxidation of propylene by a hydroperoxide complex with molybdenum catalyst.

Uses:

Polyols for urethane foams Propylene glycols Surfactants and detergents Isopropanol amines Fumigant Synthetic lubricants Synthetic elastomer (homopolymer) Solvent

Tables E-93 through E-105 and Figure E-7 present propylene oxide production, consumption, and emission data.

Storage:

Carbon steel or stainless steel should be used. Teflon-filled spiral-wound stainless steel or glass-filled Teflon can be used for gaskets or seals. Should be protected against physical damage. Detached outside storage is preferred. Inside storage should be in a standard flammable liquids storage room or cabinet. Keep isolated from combustible materials and oxidizing agents. Propylene oxide tanks should be insulated, protected by sprinklers, diked, and electrically grounded. An inert gas such as nitrogen or methane should be kept over the oxide during storage and transfer.

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Company	Location	1978 capacity, 10 ⁶ lb/yr	Process ^a	1978 production, ^b 10 ⁶ 1b/yr	Geographical coordinates, latitude/longitude
BASF Wyandotte	Wyandotte, MI	175	А	109	42 12 55/83 08 35
Dow Chemical	Freeport, TX Plaquemine, LA	1100 340	A A	684 212	28 59 35/95 23 36 30 19 00/91 15 32
Jefferson	Port Neches, TX	150	А	93	29 57 50/93 56 00
01in	Brandenburg, KY	130	А	81	38 00 27/86 06 50
Oxirane	Bayport, TX Channelview, TX	920 400	B B	572 249	29 37 26/95 03 07 29 48 50/95 07 30
To	otal	3215		2000	

TABLE E-93. PROPYLENE OXIDE PRODUCERS

^a A = chlorohydrin B = peroxidation

^b Based on 62.2% production to capacity ratio.

Source: Systems Applications, Inc. 1980.

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Source	Usage, 10 ⁶ 1b/yr	Percent usage
Urethane polyols	1120	56
Propylene glycol	480	24
Surfactant polyols	120	6
Dipropylene glycol	100	5
Glycol ethers	40	2
Miscellaneous	40	2
Exports	100	5
Total	2000	100

TABLE E-94. PROPYLENE OXIDE END-USES 1978

Source: Systems Applications, Inc. 1980.

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TABLE E-95. PROPYLENE OXIDE USERS FOR GLYCOL ETHERS PRODUCTION

Company	Location	Propylene oxide used, ^a 10 ⁶ lb/yr	Geographic location, latitude/longitude
Dow Chemical	Freeport, TX	19.5	28 59 35/95 23 36
	Plaquemine, LA	13.0	30 19 00/91 15 32
Olin	Brandenburg, KY	7.5	38 08 27/86 06 50
	Total	40.0	

^a Propylene oxide use allocated over the three sites based on ethylene glycol ethers capacity in the absence of propylene glycol ether figures.

Source: Systems Applications, Inc. 1980.

Company	Location	1978 urethane polyols capacity, 10 ⁶ lb/yr	1978 propylene oxide used, 10 ⁶ lb/yr	Geographical coordinates, latitude/longitude
BASF Wyandotte	Geismar, LA	100	45	30 11 34/91 00 42
-	Washington, NJ	40	18	40 45 20/74 58 22
	Wyandotte, MI	225	101	42 12 55/83 08 35
E. R. Carpenter Co.	Bayport, TX	150	68	29 43 20/94 54 00
Dow Chemical	Freeport, TX	400	180	28 59 35/95 23 36
	Midland, MI	20	9	43 34 08/84 16 26
Emery Industries	Mauldin, SC	10	4.5	34 48 16/82 16 09
	Santa Fe Springs, CA	10	4.5	33 55 30/118 05 40
Hodag Chemical Co.	Skokie, IL	10	4.5	42 01 50/87 43 39
Magna Corporation	Houston, TX	12	5	29 40 10/95 23 30
Milliken	Inman, SC	3	1.5	34 56 10/82 06 29
3M	Decatur, AL	15	7	34 38 39/87 02 25
Mobay Chemical	[·] Baytown, TX	100	45	29 45 30/94 54 25
	New Martinsville, WV	80	36	39 44 50/80 50 55
Malco Chemical Co.	Sugar Land, TX	40	18	29 37 10/95 38 32
Olin Corporation	Brandenburg, KY	220	100	38 08 27/86 06 50
	Lake Charles, LA	30	14	30 13 85/93 15 57
Owens-Corning	Newark, OH	10	4.5	40 05 30/82 26 00
Pelron Corporation	Lyons, IL	22	10	41 44 56/87 49 04
Petrolite Corp.	Brea, CA	15	7	33 53 30/117 58 45
	St. Louis, MO	15	7	38 41 50/90 12 08
PPG Industries, Inc.	Circleview, OH	30	14	39 36 05/82 57 34
The Quaker Oats Co.	Memphis, TN	10	4.5	35 10 30/90 56 56
Reichold	Carteret, NJ	20	9	40 35 56/74 13 13
Jefferson Chemical Co.	Austin, TX	33	15	30 20 00/97 14 15
	Conroe, TX	33	15	30 18 50/95 23 06
	Port Neches, TX	34	15	29 57 50/93 56 00
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TABLE E-96. PROPYLENE OXIDE USERS FOR URETHANE POLYOLS PRODUCTION

(continued)

TABLE E-96 (continued)

Company	Location	1978 urethane polyols capacity, 10 ⁶ lb/yr	1978 propylene oxide used, 10 ⁶ lb/yr	Geographical coordinates, latitude/longitude
Union Carbide	Institute, WV	245	110	38 23 02/81 47 24
	Seadrift, TX	245	110	28 30 31/96 46 18
	S. Charleston, WV	250	113	38 22 13/81 40 44
Upjohn .	LaPorte, TX	14	6	29 42 44/95 04 45
Witco	Clearing, IL	25	11	41 48 02/87 46 39
	Houston, TX	18	8	29 34 45/95 26 00
	Total	2484	1120	

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Source: Systems Applications, Inc. 1980.

Company	Location	Dipropylene glycol/tripropyl- ene glycol pro- duction capacity, 10 ⁶ lb/yr	Propylene oxide used, 10 ⁶ lb/yr	Geographical coordinates, latitude/longitude
Dow Chemical	Freeport, TX Plaquemine, LA	27.5 17.6	32.3 20.7	28 59 35/95 23 36 30 19 00/91 15 32
Olin	Brandenburg, KY	5	5.9	38 08 27/86 06 50
Oxirane	Bayport, TX	18	21.1	29 37 26/95 03 07
Jefferson	Port Neches, TX	7	8.2	29 57 50/93 56 00
Union Carbide	Institute, WV S. Charleston, WV	5 ^b 5 ^b	5.9 5.9	38 23 02/81 47 24 38 22 13/81 40 44
	Total	85.1	100.0	

TABLE E-97. PROPYLENE OXIDE USERS FOR DIPROPYLENE AND TRIPROPYLENE GLYCOL PRODUCTION

^aTotal propylene oxide used allocated per site based on the rate of dipropylene/tripropylene glycol individual site production capacity to total industry production capacity.

^b Capacity of 10 million lb/yr equally distributed between the two sites.

Source: Systems Applications, Inc. 1980.

Company	Location	Polyether polyols capacity, 10 ⁶ lb/yr	Propylene oxide used, 10 ⁶ lb/yr	Geographical coordinates, latitude/longitude
Emery Industries	Sante Fe Springs, CA	10	2	33 55 30/118 05 40
Olin	Brandenburg, KY	270	51	38 08 26/86 06 50
Petrolite	Brea, CA St. Louis, MO	15 ^b 15 ^b	3 3	33 53 30/117 58 45 38 41 50/90 12 08
Sherex	Janesville, WI	5	1	42 40 47/89 00 30
Union Carbide	Institute, WV Seadrift, TX S. Charleston, WV	100 ^C 100 ^C 100 ^C	19 19 19	38 23 02/81 47 24 28 30 31/96 46 18 38 22 13/81 40 44
Witco	Houston, TX	18	3	29 34 45/95 26 00
	Total	633	120	

TABLE E-98. PROPYLENE OXIDE USERS FOR SURFACTANT POLYOLS PRODUCTION

^aTotal propylene oxide used distributed over each site based on polyether polyols capacity.

^b Total capacity of 30 million 1b equally distributed between both sites.

^C Total capacity of 300 million 1b equally distributed between all three sites.

Source: Systems Applications, Inc. 1980.

Company	. Location	1978 propylene glycol capacity, 10 ⁶ lb/yr	1978 propylene oxide used, ^a 10 ⁶ lb/yr	Geographical coordinates, latitude/longitude
Dow Chemical	Freeport, TX Plaquemine, LA	250 160	140 91	28 59 35/95 23 36 30 19 00/91 15 32
Jefferson	Port Neches, TX	50	28	29 57 50/93 56 00
Olin	Brandenburg, KY	45	25	38 08 27/86 06 50
Oxirane	Bayport, TX	250	140	29 37 26/95 03 07
Union Carbide	Institute, WV S. Charleston, WV	50 50	28 28	38 23 02/81 47 24 38 22 13/81 40 44
	Total	855	480	

TABLE E-99. PROPYLENE OXIDE USERS FOR PROPYLENE GLYCOL PRODUCTION

Source: Systems Applications, Inc. 1980.

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Source	Estimated 1978 emissions, 1b/yr
Production Urethane polyols Propylene glycol Surfactant polyols Dipropylene/tripropylene glycols Glycol ethers Miscellaneous Exports	1,160,660 147,840 13,920 15,840 2,900 1,160 3,840 ^a 0
Total	1,346,160

TABLE E-100. 1978 PROPYLENE OXIDE NATIONWIDE EMISSIONS

^a Derived based on weighted average of other users except exports.

Source: Systems Applications, Inc. 1980.

		Process vent	Fugitive	Total emissions	
Company	Location	lb/yr	lb/yr	1b/yr	g/s
Dow Chemical	Freeport, TX Plaquemine, LA	1450 945	50 35	1500 980	0.022 0.014
Jefferson	Port Neches, TX	230	10	240	0.003
Olin	Brandenburg, KY	375	15	390	0.006
Oxirane	Bayport, TX	590	20	610	0.009
Union Carbide	Institute, WV S. Charleston, WV	165 165	5 5	170 170	0.002
	Total	3920	140	4060	

TABLE E-101. EMISSIONS FROM DIPROPYLENE GLYCOL, TRIPROPYLENE GLYCOL, AND GLYCOL ETHER PRODUCERS

Source: Systems Applications, Inc. 1980.

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		Process	Storage	Fugitive	Total e	missions
Company	Location	lb/yr	lb/yr	lb/yr	lb/yr	g/s
Emery	Santa Fe Springs, CA	260	Nil	Nil	265	0.004
01in	Brandenburg, KY	6,630	50	50	6,730	0.097
Petrolite	Brea, CA St. Louis, MO	390 390	Nil Nil	Ni] Ni]	395 395	0.006 0.006
Sherex	Janesville, WI	130	Nil	Nil	130	0.002
Union Carbide	Institute, WV Seadrift, TX S. Charleston, WV	2,470 2,470 2,470	20 20 20	20 20 20	2,510 2,510 2,510	0.036 0.036 0.036
Witco	Houston TX	390	Nil	Nil	395	0.006
	Total	15,600	110	110	15,840	

TABLE E-102. EMISSIONS FROM SURFACTANT POLYOL PRODUCERS

Source: Systems Applications, Inc. 1982.

		Process vent Fugitive		Total emissions	
Company	Location	emissions, lb/yr	emissions, lb/yr	lb/yr	g/s
Dow Chemical	Freeport, TX Plaquemine, LA	3,920 2,550	140 90	4,060 2,640	0.058 0.038
Jefferson	Port Neches, TX	785	30	815	0.012
Olin	Brandenburg, KY	700	25	725	0.010
Union Carbide	Instítute, WV S. Charleston, WV	785 785	30 30	815 815	0.012 0.012
	Total	9,525	345	9,870	

TABLE E-103.EMISSIONS FROM PROPYLENE OXIDE USERS FOR
PROPYLENE GLYCOL PRODUCTION

Source: Systems Applications, Inc. 1982.

		Proce ve emis	ess nt sions	Stori vei emis:	age nt sions	Fug emis	itive sions	Tot emissi	al Ons	-		
Company	Location	lb/yr	g/s	lb/yr	g/s	lb/yr	- 1 -	1h/un	۵/۹	-		
BASF Wyandotte E. R: Carpenter Co. Dow Chemical Emery Industries Hodag Chemical Co. Magna Corporation Milliken Minnesota Mining & Manufacturing Mobay Chemical Nalco Chemical Co. Olin Owens-Corning Pelron Corporation Petrolite Corp. PPG Industries, Inc. The Quaker Oats Co. Reichold Jefferson Chemical Co. Union Carbide	Geismar, LA Washington, NJ Wyandotte, MI Bayport, TX Freeport, TX Midland, MI Mauldin, SC Santa Fe Springs, CA Skokie, IL Houston, TX Inman, SC Decatur, AL Baytown, TX New Martinsville, WV Sugar Land, TX Brandenburg, KY Newark, OH Lyons, IL Brea, CA St. Louis, MO Circleview, OH Memphis, TN Carteret, NJ Austin, TX Conroe, TX Port Neches, TX Institute, WV Seadrift, TX S. Charleston, WV LaPorte TX	103,703 2,400 13,200 8,800 23,400 1,200 600 600 600 200 1,000 5,800 4,600 2,400 1,00	1.49 0.03 0.19 0.13 0.34 0.02 0.01 0.01 0.01 0.01 0.01 0.03 0.01 0.03 0.01 0.02 0.01 0.02 0.03 0.03 0.03 0.03 0.03 0.21 0.21 0.01	708 20 100 80 100 40 20 100 20 20 20 20 20 20 20 20 20 20 20 20 2	0.10 0.002 0.001 0.002 0.002 0.001 0.002 0.002 0.002 0.002	40 20 80 60 140 40 20 20 80 20 20 20 20 20 20 20 20 80 80 80 80	86/98	ŝ	anneal and	have for chettane	From Propylane Pride	Table E-108 Emissione
Witco	Clearing, IL Houston, TX	1,400 1,000	0.02 0.01	20				1,420 1,000	0.02			
	Total	241,903		1,688		820		244,411		-		

TABLE E-104. EMISSIONS FROM PROPYLENE OXIDE USERS FOR URETHANE POLYOLS PRODUCTION^a

Source: Systems Applications, Inc. 1980.

			Process vents ^a						
		f	Stack height, m	Stack	Stack	Storage vent emissions, lb/yr	Fugitive emissions, lb/yr	Total emissions	
Company	Location	ib/yr		arameter, m	°C			1b/yr	g/s
BASF Wyandotte	Wyandotte, MI	81,750	10.4	0.26	25	3,380	2,290	87,420	1.25
Dow Chemical	Freeport, TX Plaquemine, LA	513,000 159,000	10.4 10.4	0.26 0.26	25 25	21,200 6,570	14,360 4,450	548,560 170,020	7.89 2.45
Jefferson	Port Neches, TX	69,750	7.25	0.19	46	2,860	1,950	74,560	1.07
Olin	Brandenburg, KY	60,750	10.4	0.26	25	2,510	1,700	64,960	0.94
Oxirane	Bayport, TX Channelview, TX	120,120 52,290	9.1 14.6	0.05 0.76	21 26	17,730 7,720	12,010 5,230	149,860 65,240	2.16 0.94
	Total	1,056,660				61,970	41,990	1,160,620	

TABLE E-105. EMISSIONS FROM PROPYLENE OXIDE PRODUCERS

^a Stack velocity for all plants 2 m/s.

Source: Systems Applications, Inc. 1980.



NOTE: NUMERALS DENOTE NUMBER OF PLANTS.

Figure E-7. Specific point sources of propylene oxide emissions.

Source: Systems Applications, Inc., 1980.

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Transportation:

Shipped in glass bottles, cans, metal drums, tank trucks, tank cars, tank barges, and cargo ships, usually with nitrogen over the propylene oxide. Must be labeled "Flammable Liquid." Shipment by ship must be kept under an inert gas pad and maintained at or below 40°C.

Disposition:

Propylene oxide may be disposed of as a concentrated waste containing no peroxides by discharge of the liquid at a controlled rate near a pilot flame or as a concentrated waste containing peroxides by perforation of a container of the waste from a safe distance followed by open burning.

Sampling and Analytical Methods

- 1. NIOSH Method S75
 - a. Adsorption with charcoal.
 - b. Desorption with carbon disulfide.
 - c. Gas chromatography.

Sampling and Analytical Methods

- 1. NIOSH Method S75
 - a. Adsorption with charcoal.
 - b. Desorption with carbon disulfide.
 - c. Gas chromatography.

Detection limit: 25 to 720 mg/m³ (10 to 288 ppm) for a 5-liter sample

Possible interferences:

High humidity may hamper vapor trapping efficiency. Any compound with the same retention time as propylene oxide will cause interference.

- 2. Method B (Appendix A): C_2-C_{18} hydrocarbons and other nonpolar organics with a boiling point of 100° to 175°C.
 - a. Whole air collection in canister.
 - b. Cryogenic concentration.
 - c. Gas chromatography/flame ionization detection.

Detection limit:

0.1 ppb per 100-ml sample

Possible interferences:

Water-soluble compounds are not readily analyzed. Storage times greater than a week are not recommended.

Method C (Appendix A): C_6-C_{12} hydrocarbons and other nonpolar 3. organics with a boiling point between 60° and 200°C. a. Adsorption on Tenax. b. Thermal desorption. c. Gas chromatography/mass spectrometry analysis. Detection limit: 1 to 200 ppt for a 20-liter sample Possible interferences: Blank levels usually limit sensitivity artifacts due to reactive components $(0_3, NO_2)$. Sample can be analyzed only once. Low breakthrough volume on Tenex adsorption. 4. Method D (Appendix A): C_6-C_{12} hydrocarbons and other nonpolar organics with a boiling point of 60° to 200°C. a. Adsorption on Tenax. b. Thermal desorption into canisters. c. Gas chromatography/flame ionization detection, or gas chromatography/mass spectrometry analysis. Detection limit: 0.01 to 1 ppb for a 20-liter sample Possible interferences:

Blanks and artifact problems in Method C, above low breakthrough volume on Tenex adsorption.

Permissible Exposure Limits

	OSHA	ACGIH		
TWA	100 ppm (240 mg/m ³)	20 ppm (50 mg/m ³)		

Human Toxicity

Acute Toxicity: Skin and eye irritant. A food additive permitted in food for human consumption.

Chronic Toxicity:

s.

Propylene oxide was found to be carcinogenic in rats in a limited study in which subcutaneous injection produced sarcomas. No epidemiological studies were found.

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Chemical Name

o-, m-, p-xylene (where properties differ, they are presented in o-, m-, p- order)

CAS Number

95-47-6; 108-38-3; 106-42-3; mixed isomers 1330-20-7

Chemical Classification

Aromatic hydrocarbon, alkyl benzene

Synonyms

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(o-,m-,p-) dimethylbenzene; 1, (2-,3-,4-,) dimethylbenzene;
(o-,m-,p-,) methyltoluene; 1 (2-,3-,4-) xylene; (o-,m-,p-) xylol
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Physical/Chemical Properties

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Description:
     Clear colorless liquid; p-xylene exists as crystals at low
     temperature.
Boiling Point:
     144°C; 138.8°C; 138.5°C
Melting Point:
      -25°C; -47.4°C; 13.2°C
Molecular Weight:
     106.2
Chemical Formula:
     1, (2-,3-,4-) C<sub>6</sub>H<sub>4</sub>(CH<sub>3</sub>)<sub>2</sub>
Vapor Pressure:
     10 mm Hg at 32.1°C; 10 mm Hg at 28.3°C; 10 mm Hg at 27.3°C
Vapor Density:
     3.66 (air = 1.0)
Refractive Index:
     N_{D}^{20} = 1.505; N_{D}^{20} = 1.497; N_{D}^{20} = 1.500
Solubility:
     Soluble in alcohol and ether, insoluble in water.
Log Partition Coefficient (octanol/water):
     2.77; 3.20; 3.15
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Photochemical Reactivity:

Transformation products are formaldehyde, acetaldehyde, PAN, and benzaldehyde. Xylene can be easily chlorinated, sulfonated, and nitrated. Reactivity toward OH· has a half-life of 3 days (8 times butane) for m and p; o has a half-life of 6 days. Reactivity toward O_3 has no reaction for o and m; half-life 100 years for p.

Chemical Reactivity:

Contact with strong oxidizers may cause fires and explosions. Toxic gases and vapors (such as carbon monoxide) may be released in a fire involving xylene. Elevated temperatures may cause containers to burst. p-xylene incompatible with acetic acid + air; HNO₃; and 1,3-dichloro-3,5-dimethyl-2,4-imidazolidindione. Xylene will attack some forms of plastics, rubber, and coatings.

Environmental Fate

Calculated half-life in water at a depth of 1 meter at 25°C is 5.6 hours based on evaporative loss from the water. Some half-lives for photochemical reactions in air are presented in the photochemical reactivity section. Estimated overall lifetime under photochemical smog conditions in southeastern England is 2 to 6 hours.

Source of Emissions

Production:

Selective crystallization or solvent extraction from meta-para mixtures.

Uses:

Solvent Intermediate for dyes and organic synthesis especially for isophthalic acid Insecticides Aviation fuel

Tables E-106 through E-119 and Figure E-8 present data on xylene production, consumption, and emissions.

Storage:

Should be protected against physical damage. Outside or detached storage is preferable. Inside storage should be in a standard flammable liquids storage room or cabinet, separate from oxidizing materials.

Transportation:

Shipped in glass containers in 55- and 110-gallon metal drums; in tank cars and tank trucks; and on tank barges.

Disposition:

Xylenes may be disposed of by incineration

TABLE E-106. XYLENE ISOMER PRODUCERS

Company	Location	Isomer capacity, 10 ⁵ lb/yr	Isomer production, 10 ⁶ lb/yr	Geographic coordinates, Latitude/longitude
o-xylene Producers				
ARCO	Houston, TX	210	183	29 42 17/95 16 01
Corco	Ponce, PR	175	153	Not in project scope
Exxon	Baytown, TX	200	174	29 44 50/95 01 00
Monsanto	Chocolate Bayou, TX	30	26	29 14 55/95 12 45
Phillips	Guayama, PR	130	113	Not in project scope
Shell	Deer Park, TX	165	144	29 42 55/95 07 34
Sun	Corpus Christi, TX	160	140	27 49 53/97 31 30
Tenneco	Chalmette, LA	130	113	30 03 30/89 58 30
Total		1200	1046	
m-xylene Producer				
Атосо	Texas City, TX	175	88	29 21 40/94 55 50
p-xylene Producers				
Атосо	Decatur, AL Texas City, TX	1300 900	952 659	34 36 12/86 58 42 29 21 40/94 55 50
Arco	Houston, TX	360	264	29 42 17/95 16 01
Chevron	Pascagoula, MS	330	242	30 19 04/88 28 37
St. Croix	St. Croix, VI	600	440	Not in project scope

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TABLE E-106 (continued)

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Company	Location	Isomer capacity, 10 ⁶ lb/yr	Isomer production, 10 ⁶ lb/yr	Geographic coordinates, Latitude/longitude
p-xylene Producers	(cont.)			
Exxon	Baytown, TX	420	308	29 44 50/95 01 00
Hercor	Penuelas, PR	600	440	Not in project scope
Phillips	Guayama, PR	470	344	Not in project scope
Shell	Deer Park, TX	110	80	29 42 55/95 07 34
Sun	Corpus Christi, TX	390	286	27 49 53/97 31 30
Tenneco	Chalmette, LA	125	92	30 03 30/89 58 30
Total		5605	4107	
Ethylbenzene Produc	cers ^a			
ARCO	Houston, TX	136	99	29 42 17/95 16 01
Charter	Houston, TX	35	25	29 42 50/95 15 12
Monsanto	Chocolate Bayou, TX	59	43	29 14 55/95 12 45
Sun	Corpus Christi, TX	73	53	27 49 53/97 31 30
Total		303	220	

^aEthylbenzene is considered to be a mixed xylene isomer.

Source: Systems Applications, Inc., 1980.

Source	Isolated mixed xylene product, 10 ⁶ lb/yr	Nonisolated mixed xylene production, 10 ⁶ lb/yr	Total mixed xylene production, 10 ⁶ lb/yr
Catalytic reformate	7,991	68,925	76,916
Pyrolysis gasoline	429	397	826
Toluene disproportionation	106	92	198
Coal-derived	29	4	33
Total	8,555	69,418	77,973

	TABLE	E-107.	MIXED	XYLENE	PRODUCTION	SOURCE	SUMMARY
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Source: Systems Applications, Inc., 1980.

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Company	Location	Mixed xylene capacity, metric tons/yr	Isolated mixed xylene produced, 10 ⁶ lb/yr	Geographic coordinates, Latitude/longitude
Amerada Hess	St. Croix, VI	457	699	Not in project scope
American Petrofina	Big Spring, TX Beaumont, TX	209 49	306 72	32 17 10/101 25 17 29 57 30/93 53 20
Ashland Oil	Catlettsburg, KY N. Tonawanda, NY	98 46	143 67	38 22 39/82 35 58 42 59 45/78 55 27
ARCO	Houston, TX	258	378	29 42 17/95 16 01
Charter Oil	Houston, TX	36	53	29 42 50/95 15 12
Cities Service	Lake Charles, LA	163	239	30 10 58/93 19 01
Coastal States	Corpus Christi, TX	55	80	27 48 43/97 26 28
Commonwealth	Penuelas, PR	343	502	Not in project scope
Crown	Pasadena, TX	46	67	29 44 40/95 10 30
Exxon	Baytown, TX	408	597	29 44 50/95 01 04
Gulf	Alliance, LA	196	287	29 50 00/90 00 10
Kerr McGee	Corpus Christi, TX	140	205	27 48 15/97 25 24
Marathon	Texas City, TX	36	53	29 22 22/94 54 58
(continued)	1	I	1	1

TABLE E-108. ISOLATED MIXED XYLENE PRODUCTION FROM CATALYTIC REFORMATE

TABLE E-108 (continued)

Company	Location	Mixed xylene capacity, metric tons/yr	Isolated mixed xylene produced, 10 ⁶ lb/yr	Geographic coordinates, Latitude/longitude
Monsanto	Texas City, TX	32	47	29 22 45/94 33 30
Phillips	Guayama, PR	326	477	Not in project scope
Quitana-Howell	Corpus Christi, TX	42	61	27 48 35/97 27 30
Shell	Deer Park, TX	245	359	29 42 55/95 07 33
Chevron	Pascagoula, MS Richmond, CA	212 196	310 287	30 19 04/80 28 37 37 56 12/122 20 48
Amoco	Texas City, TX Whiting, IN	800 588	1,171 860	29 21 40/94 55 50 41 41 07/87 29 02
Sun	Corpus Christi, TX Marcus Hook, PA Toledo, OH	78 65 163	114 95 239	27 49 53/97 31 30 39 48 45/75 24 51 41 36 52/83 31 40
Tenneco	Chalmette, LA	130	190	30 03 30/89 58 30
Union Oil	Chicago, IL	33	48	41 38 33/88 03 02
Union Pacific	Corpus Christi, TX	10	15	27 48 10/97 35 29
Total		5,460	8,021	

Source: Systems Applications, Inc., 1982.

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Region	Number of sites	Reformate capacity, 10 ⁶ bbl/day	Non- isolated mixed xylene produced, 10 ⁶ lb/yr	Average nonisolated mixed xylene produced per site, 10 ⁶ lb/yr
New England	0	0	0	0
Middle Atlantic	17	369,952	6,743	397
East North Central	28	624,178	11,377	406
West North Central	16	165,250	3,012	188
South Atlantic	5	57,660	1,051	210
East South Central	8	144,700	2,637	330
West South Central	71	1,649,303	30,061	423
Mountain	23	123,094	2,243	98
Pacific	33	647,461	11,801	358
Total	201	3,781,598	68,925	343

TABLE E-109. NONISOLATED MIXED XYLENE (AS BTX) PRODUCTION FROM CATALYTIC REFORMATE

Source: Systems Applications, Inc., 1980.

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Company	Location	Production capacity, 10 ⁶ 1b/yr	Non- isolated mixed xylene produced, 10 ⁶ lb/yr	Isolated mixed xylene produced, 10 ⁶ lb/yr	Total mixed xylene produced, 10 ⁶ lb/yr	Geographic coordinates, Latitude/longitude
Pyrolysis gasoline						
ARCO	Channelview, TX	1179	79	168	247	29 50 04/95 06 43
Lommonwealth	Penuelas, PR	454	30	91	121	
Exxon	Baton Rouge, LA	816	55		55	30 09 10/90 54 20
Gulf	Cedar Bayou, TX	544	37		37	29 49 29/94 55 10
Mobile	Beaumont, TX	408	27		27	30 04 00/94 03 30
Monsanto	Texas City, TX	340	23	61	84	29 15 00/95 12 40
Shell	Deer Park, TX	624	42	100	42	29 42 55/95 07 33
Union Carbide	laft, LA	41/	28	109	137	29 58 00/90 27 00
Total		5916	397	429	826	
Coal-derived						
Ashland	Catlettsburg, KY	13	1.6	11.4	13	38 22 39/82 35 58
	N. Tonawanda, NY	7	0.8	6.2	7	42 59 45/78 55 27
U.S. Steel	Clairton, PA	13	1.6	11.4	13	40 18 15/79 52 43
Total		33	4.0	29.0	33	
Toluene dispro- portionation						
ARCO	Houston. TX	196	45	52	97	29 42 17/95 16 01
Sun	Marcus Hook, PA	202	47	54	101	39 48 45/75 24 51
Total		398	92	106	198	

TABLE E-110. OTHER MIXED XYLENE PRODUCERS

NA = Not applicable.

Source: Systems Applications, Inc. 1980.

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	Usa	ge
	10 ⁶ 1b/yr	%
Mixed xylene as BTX (not isolated)	69,418	
Gasoline	69,418	100.0
Isolated mixed xylene	8,555	
p-xylene isomer o-xylene isomer m-xylene isomer Ethylene benzene Gasoline backblending Paint and coating solvent Adhesives solvent Chemical manufacturing solvent Agricultural solvent Other miscellaneous solvents Net export	4,107 1,046 88 220 2,158 496 77 77 66 55 165	48.0 12.2 1.0 2.6 25.2 5.8 0.9 0.9 0.9 0.9 0.8 0.7 1.9
o-xylene	1,046	
Phthalic anhydride Gasoline backblending Exports	670 21 355	64.1 2.0 33.9
p-xylene	4,107	
Terephthalic acid Dimethyl terephthalate Net exports Gasoline backblending	1,430 2,040 620 17	34.8 49.7 15.1 0.4
m-xylene	88	
Isophthalic acid	98 ^a	100.0

TABLE E-111. END-USE DISTRIBUTION - 1978 MIXED XYLENE AND XYLENE ISOMERS

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^aDifference between production and use supplied by imports.

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Source: Systems Applications, Inc., 1980.

Company	Location	Production capacity, 10 ⁶ lb/yr	o-Xylene used, 10 ⁶ lb/yr	Geographic coordinates, Latitude/longitude
·	Phtha	lic Anhydride Proc	lucers (o-xylene)	
Allied	El Segundo, CA	36	26	33 56 30/118 26 35
BASF Wyandotte	Kearny, NJ	150	107	40 45 53/74 09 03
Exxon	Baton Rouge, LA	130	93	30 09 10/90 54 20
Koppers	Cicero, IL	235	168	41 48 44/87 45 04
Monsanto	Texas City, TX	150	107	29 22 45/94 33 30
Hooker	Arecibo, PR	87	62	Not in project scope
Chevron	Richmond, CA	50	36	37 56 12/122 20 48
Stepan	Millsdale, IL	100	71	41 26 03/88 09 48
Total		938	670	
	Isop	hthalic Acid Produ	cer (m-xylene)	
Amoco	Joliet, IL	240	98	41 26 48/88 10 41
(continued)				

TABLE E-112. XYLENE ISOMER END-USERS

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TABLE E-112 (continued)

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Location	Production capacity, 10 ⁶ lb/yr	o-Xylene used, 10 ⁶ lb/yr	Geographic coordinates, Latitude/longitude
Dimethylte	erephthalic Acid F	Producers (o-xylen	e)
Old Hickory, TN Wilmington, NC	550 1250	273 622	36 16 24/86 34 12 34 10 00/77 56 06
Columbia, SC Kingsport, TN	500 500	249 249	33 59 50/81 04 17 36 31 41/82 12 22
Wilmington, NC	1300	647	34 19 27/77 46 56
	4100	2040	
Tereph	thalic Acid Produ	cers (p-xylene)	
Cooper River, SC Decatur, AL	1000 2000	441 883	32 45 57/79 58 28 34 36 12/86 58 42
Wilmington, NC	240	106	34 19 27/77 46 56
	3240	1430	
	Location Dimethylte Old Hickory, TN Wilmington, NC Columbia, SC Kingsport, TN Wilmington, NC Tereph Cooper River, SC Decatur, AL Wilmington, NC	LocationProduction capacity, 10 ⁶ 1b/yrDimethylterephthalic Acid FOld Hickory, TN01d Hickory, TN550Wilmington, NC1250Columbia, SCKingsport, TN500Wilmington, NC13004100Terephthalic Acid ProduCooper River, SCDecatur, AL2000Wilmington, NC2403240	Production capacity, 106 lb/yro-Xylene used, 106 lb/yrDimethylterephthalic Acid Producers (o-xylenOld Hickory, TN550Vilmington, NC1250Columbia, SC500Kingsport, TN500Wilmington, NC1300Hilmington, NC1300Coumbia, SC500Coumbia, SC500Kingsport, TN500Cooper River, SC1000Cooper River, SC1000Milmington, NC240Statur, AL2000Statur, AL2000Statur, AL240Statur, AL240Statur, AL1430

Source: Systems Applications, Inc., 1980.

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	Nationwide emissions, lb/yr
<u>p-xylene</u>	
Mixed xylene production Mixed xylene solvent use Ethyl benzene production p-Xylene production Terephthalic acid production Dimethylterephthalate production Gasoline marketing - evaporation Gasoline automobile - evaporation	1,610,076 114,395,000 7,348 6,447,990 469,200 3,889,600 2,138,500 1,967,100 108,345,600
Total	239,270,414
<u>o-xylene</u>	
Mixed xylene production Mixed xylene solvent use Ethyl benzene production o-Xylene production Phthalic anhydride Gasoline marketing - evaporation Gasoline automobile - evaporation Gasoline automobile - exhaust Total	1,976,440 140,425,000 9,020 2,667,300 134,000 2,138,500 1,967,100 119,180,000 268,497,360
<u>m-xylene</u>	
Mixed xylene production Mixed xylene solvent use Ethyl benzene production m-Xylene production Isophthalic acid Gasoline marketing - evaporation Gasoline automobile - evaporation Gasoline automobile - exhaust	3,706,331 244,545,000 15,708 176,000 98,000 5,193,400 4,777,400 195,022,100
<u>Gasoline automobile - exhaust</u> Total	195,022,1

TABLE	E-113.	1978	NATIONWIDE	EMISSIONS	0F	XYLENE	ISOMERS

Source: Systems Applications, Inc., 1980.

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		Em	issions, 1b/y	/r	Total emi	ssions
Company	Location	Process	Storage	Fugitive	lb/yr	g/s
o-xylene Producers						
ARCO Corco Exxon Monsanto Phillips Shell Sun Tenneco	Houston, TX Ponce, PR Baytown, TX Chocolate Bayou, TX Guayama, PR Deer Park, TX Corpus Christi, TX Chalmette, LA	382,470 319,770 363,660 54,340 237,170 300,960 292,600 236,170	14,640 12,240 13,920 2,080 9,040 11,520 11,200 9,040	69,540 58,140 66,120 9,880 42,940 54,720 53,200 42,940	466,650 390,150 443,700 66,300 289,150 367,200 357,000 288,150	6.72 5.62 6.39 0.95 4.15 5.28 5.14 4.15
Total		2,187,140	83,680	397,480	2,668,300	
m-xylene Producer						
Amoco	Texas City, TX	139,040	10,560	26,400	176,000	2.53
p-xylene Producers						
Amoco ARCO Chevron St. Croix Exxon Hercor Phillips Shell Sun Tenneco	Decatur, AL Texas City, TX Houston, TX Pascagoula, MS St. Croix, VI Baytown, TX Penuelas, PR Guayama, PR Deer Park, TX Corpus Christi, TX Chalmette, LA	1,085,280 751,260 300,960 275,880 501,600 351,120 501,600 392,160 91,200 326,040 104,880	180,880 125,210 50,160 45,980 83,600 58,520 83,600 65,360 15,200 54,340 17,480	228,480 158,160 63,360 58,080 105,600 73,920 105,600 82,560 19,200 68,640 22,080	1,494,640 1,034,630 414,480 379,940 690,800 483,560 690,800 540,080 125,600 449,020 144,440	21.52 14.89 5.97 5.47 9.94 6.96 9.94 7.78 1.81 6.46 2.08
Total		4,681,980	780,330	985,680	6,447,990	

TABLE E-114. XYLENE ISOMER EMISSIONS FROM XYLENE ISOMER PRODUCERS

Source: Systems Applications, Inc., 1980.

		Emissions, 1b/yr			Total emissions	
Company	Location	Process	Storage	Fugitive	lb/yr	g/s
Pyrolysis-Gasoline						
ARCO	Channelview, TX	17,290	74,100	7,410	98,800	1.42
Commonwealth	Penuelas, PR	8,470	36,300	3,630	48,400	0.70
Dow	Freeport, TX	5,320	22,800	2,280	30,400	0.44
Exxon	Baton Rouge, LA	3,850	16,500	1,650	22,000	0.32
Gulf	Cedar Bayou, TX	2,590	11,100	1,110	14,800	0.21
Mobile	Beaumont, TX	1,890	8,100	810	10,800	0.16
Monsanto	Texas City, TX	5,880	25,200	2,520	33,600	0.48
Shell	Deer Park, TX	2,940	12,600	1,260	16,800	0.24
Union Carbide	Taft, LA	9,590	41,100	4,110	54,800	0.79
Total		57,820	247,800	24,780	330,400	
Coal-Derived						
Ashland	Catlettsburg, KY N. Tonawanda, NY	6,500 3,500	7,800 4,200	1,950 1,050	16,250 8,750	0.23 0.13
U.S. Steel	Clairton, PA	6,500	7,800	1,950	16,250	0.23
Total		16,500	19,800	4,950	41,250	
Toluene Disproportionation						
ARCO	Houston, TX	4,850	9,700	4,850	19,400	0.29
Sun	Marcus Hook, PA	5,050	10,100	5,050	20,200	0.30
Total		9,900	19,800	9,900	39,600	

TABLE E-115. MIXED XYLENE EMISSIONS FROM OTHER MIXED XYLENE PRODUCERS

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		Emissions, 1b/yr			Total emissions	
Company	Location	Process	Storage	Fugitive	lb/yr	g/s
Amerada Hess	St. Croix, VI	20,070	40,140	20,070	80,280	1.16
American Petrofina	Big Springs, TX Beaumont, TX	9,180 2,160	18,360 4,320	9,180 2,160	36,720 8,640	0.53 0.12
Ashland Oil	Catlettsburg, KY N. Tonawanda, NY	4,290 2,010	8,580 4,020	4,290 2,010	17,160 8,040	0.25 0.12
ARCO	Houston, TX	11,340	22,680	11,340	45,360	0.65
Charter Oil	Houston, TX	1,590	3,180	1,590	6,360	0.09
Cities Service	Lake Charles, LA	7,170	14,340	7,170	28,680	0.41
Costal States	Corpus Christi, TX	2,400	4,800	2,400	9,600	0.14
Commonwealth	Penuelas, PR	15,060	30,120	15,060	60,240	0.87
Crown	Pasadena, TX	2,010	4,020	2,010	8,040	0.12
Exxon	Baytown, TX	17,910	35,820	17,910	71,640	1.02
Gulf	Alliance, LA	8,610	17,220	8,610	34,440	0.50
Kerr-McGee	Corpus Christi, TX	6,150	12,300	6,150	24,600	0.35
Marathon	Texas City, TX	1,590	3,180	1,590	6,360	0.09
(continued)	I	I	I	ſ	1	i

TABLE E-116. MIXED XYLENE EMISSIONS FROM CATALYTIC REFORMATE (ISOLATED MIXED XYLENES) PRODUCTION

TABLE E-116 (continued)

		E	missions, 1b/	Total emissions		
Company	Location	Process	Storage	Fugitive	lb/yr	g/s
Monsanto	Texas City, TX	1,410	2,820	1,410	5,640	0.08
Phillips	Guayama, PR	14,310	28,620	14,310	57,240	0.82
Quitana-Howell	Corpus Christi, TX	1,830	3,660	1,830	7,320	0.11
Shell	Deer Park, TX	10,770	21,540	10,770	43,080	0.62
Chevron	Pascagoula, MS Richmond, CA	9,300 8,610	18,600 17,220	9,300 8,610	37,200 34,440	0.54 0.50
Атосо	Texas City, TX Whiting, IN	35,130 25,800	70,260 51,600	35,130 25,800	140,520 103,200	2.02 1.49
Sun	Corpus Christi, TX Marcus Hook, PA Toledo, OH	3,420 2,850 7,170	6,840 5,700 14,340	3,420 2,850 7,170	13,680 11,400 28,680	0.20 0.16 0.41
Tenneco	Chalmette, LA	5,700	11,400	5,700	22,800	0.33
Union Oil	Chicago, IL	1,440	2,880	1,440	5,760	0.08
Union Pacific	Corpus Christi, TX	450	900	450	1,800	0.03
Total		239,730	479,460	239,730	958,920	

Source: Systems Applications, Inc., 1980.

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		Emissions, 1b/yr			Total er	nissions
Company	Location	Process	Storage	Fugitive	lb/yr	g/s
	Phthalic A	nhydride Produ	cers (o-xyler	ne)		
Allied BASF Wyandotte Exxon Koppers Monsanto Hooker Chevron Stepan	El Segundo, CA Kearny, NJ Baton Rouge, LA Ciecero, IL Texas City, TX Arecibo, PR Richmond, CA Millsdale, IL	3,640 14,980 13,020 23,520 14,980 8,680 5,040 9,940	520 2,140 1,860 3,360 2,140 1,240 720 1,420	1,040 4,280 3,720 6,720 4,280 2,480 1,440 2,840	5,200 21,400 18,600 33,600 21,400 12,400 7,200 14,200	0.07 0.31 0.27 0.48 0.31 0.18 0.10 0.20
Total		93,800	13,400	26,800	134,000	
	Isophthal	ic Acid Produce	er (m-xylene)			
Атосо	Joliet, IL	83,000	4,900	9,800	98,000	1.41
	Dimethyltere	phthalate Produ	ucers (p-xyle	ene)		
DuPont Eastman Kodak	Old Hickory, TN Wilmington, NC Columbia, SC	35,490 87,360 32,370	8,190 18,660 7,470	19,110 43,540 17,430	62,790 149,560 57,270	0.90 2.15 0.82
Hercofina	Wilmington, NC	84,110	19,410	45,290	148,810	0.82
Total	-L	271,700	61,200	142,800	475,700	
	Terephthal	ic Acid Produce	ers (p-xylene	e)	.	· · · · · · · · · · · · · · · · · · ·
Amoco Hercofina	Cooper River, SC Decatur, AL Wilmington, NC	1,120,140 2,242,820 269,240	48,510 97,130 11,660	30,870 61,810 7,420	1,199,520 2,401,760 288,320	17.27 34.58 4.15
Total		3,632,200	157,300	100,100	3,889,600	

TABLE E-117. XYLENE ISOMER EMISSIONS FROM USERS

Source: Systems Applications, Inc., 1982.

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	Total mixed xylene emissions, 10 ⁶ lb/yr	p-xylene emissions, 10 ⁶ lb/yr	o-xylene emissions, 10 ⁶ lb/yr	m-xylene emissions, 10 ⁶ lb/yr
Paints and coatings	422	70.474	86.510	150.654
Adhesive, rubber	77	12.859	15.785	27.489
Chemical, automotive	65	10.855	13.325	23.205
Agricultural pesticides	66	11.022	13.530	23.562
Household products, printing inks	55	9.185	11.275	19.635
Total	685	114.395	140.425	244.545

TABLE E-118. XYLENE ISOMER EMISSIONS FROM MIXED XYLENE SOLVENT USES

Source: Systems Applications, Inc., 1980.

Region	Number of sites	o-xylene emissions, lb/yr	m-xylene emissions, lb/yr	p-xylene emissions, lb/yr
New England	11,105	104,831	254,638	104,831
Middle Atlantic	28,383	267,935	650,822	267,935
East North Central	42,270	399,029	969,251	399,029
West North Central	23,304	219,990	534,361	219,990
South Atlantic	37,286	351,980	854,968	351 ,9 80
East South Central	16,313	153,995	374,057	153,995
West South Central	28,336	267,492	649,744	267,492
Mountain	12,815	120,974	293,848	120,974
Pacific	26,647	251,548	611,016	251,548
Total	226,459	2,137,774	5,192,705	2,137,774

TABLE E-119. XYLENE ISOMER EMISSIONS FROM GASOLINE MARKETING

Source: Systems Applications, Inc., 1982.

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NOTE: NUMERALS DENOTE NUMBER OF PLANTS.



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Source: Systems Applications, Inc., 1980.
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Sampling and Analytical Methods

1.	NIOSH Method 1501 a. Solid Sorbent Tube (coconut shell charcoal, 100 mg/50 mg). b. Gas chromatography. c. Flame ionization detector.
	Detection limit: 0.2 ppm for 10-liter sample
	Possible interferences: Alkanes less than C ₁₀ along with volatile organic sol- vents (e.g., alcohols, keytones, ethers, and halogenated hydrocarbons).
2.	 Method B (Appendix A): C₂-C₁₈ hydrocarbons and other nonpolar organics with a boiling point of 100° to 175°C. a. Whole air collection in canister. b. Cryogenic concentration. c. Gas chromatography/flame ionization detection (gas chromatography/photoionization detection may also be used).
	Detection limit: 0.1 ppb per 100-ml sample
	Possible interferences: Reactive compounds are not readily analyzed. Storage times greater than a week are not recommended.
3.	 Method C (Appendix A): C₆-C₁₂ hydrocarbons and other nonpolar organics with a boiling point of 60° to 200°C. a. Adsorption of Tenax (XAD-2 with solvent extraction may be used). b. Thermal desorption. c. Gas chromatography/mass spectrometry analysis (gas chromatography/photoionization detection may also be used).
	Detection limit: 1 to 200 ppt for a 20-liter sample
	Possible interferences: Blank levels usually limit sensitivity artifacts due to reactive components (O ₃ , NO _x). Sample can be analyzed only once.
4.	 Method D (Appendix A): C₆-C₁₂ hydrocarbons and other nonpolar organics with a boiling point of 60° to 200°C. a. Adsorption of Tenax (XAD-2 with solvent extraction may be used). b. Thermal desorption into canisters.

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c. Gas chromatography/flame ionization detection, or gas chromatography/mass spectrometry analysis (gas chromatography/photoionization detection may also be used).

Detection limit: 0.01 to 1 ppb for a 20-liter sample

Possible interferences: Blanks and artifact problems in Method C, above.

Permissible Exposure Limits

	OSHA	ACGIH	NIOSH
TWA	100 ppm (435 mg/m ³)	100 ppm (435 mg/m ³)	100 ppm
Ceiling			200 ppm (10 min)
STEL		150 ppm (655 mg/m³)	

Human Toxicity

Acute Toxicity:

Human eye and skin irritation can start at 200 ppm. Moderate irritant through intraperitoneal, subcutaneous, and inhalation means. Low toxicity orally. Very little dermal toxicity. At high concentrations, xylene vapor may cause severe breathing difficulties, which may be delayed in onset. At high concentration, may also cause dizziness, staggering, drowsiness, and unconsciousness. In addition, breathing high concentrations may cause lack of appetite, nausea, vomiting, abdominal pain, and reversible damage to kidneys and liver.

Chronic Toxicity:

Repeated exposure of the eyes to high concentrations of xylene vapor may cause reversible eye damage.

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APPENDIX F

GUIDANCE FOR THE CHOICE OF MONITORING FREQUENCY TO BE USED IN ESTIMATING ANNUAL AVERAGE CONCENTRATIONS OF NONCRITERIA AIR POLLUTANTS

Prepared by

Systems Applications, Inc. 101 Lucas Valley Road San Rafael, California 94903

Monitoring Section Monitoring and Data Analysis Division U.S. Environmental Protection Agency Research Triangle Park, North Carolina 27711

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ABSTRACT

The reliability of the estimated annual average concentration of a noncriteria air pollutant is considered. The increase in precision resulting from more frequent monitoring is illustrated, and guidance on the selection of a monitoring frequency to achieve a desired precision is provided.

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DISCLAIMER

Although this report has been funded by the United States Environmental Protection Agency through Contract No. 68-02-3848, it has not been subject to the Agency's peer and administrative review; therefore, it does not necessarily reflect the views of the Agency, and no official endorsement should be inferred.

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INTRODUCTION

There are at present no national ambient air quality standards for a number of air pollutants considered to be of possible harm to public health. Planning is in progress, and some programs are already underway, by national, state, and local agencies, to monitor these so-called noncriteria air pollutants. The monitoring data will be used for many purposes, e.g., to estimate air quality trends, population exposure, or the influence of emissions.

In allocating funds for these programs, it is important to determine where and how often the pollutants must be monitored to achieve stated objectives. In this report we restrict attention to the sampling frequency required to reliably estimate annual average concentrations. Other monitoring objectives, as well as the costs and health henefits of various monitoring alternatives, although very important, are not discussed here. In particular, the monitoring of high concentrations of short duration will be addressed in a future report.

Our purpose is thus to quantify and illustrate the effect of sampling frequency on the precision of the sample annual average concentration of a noncriteria air pollutant. It should be noted that even within this narrowly defined context we have had to set aside from our discussion certain important aspects of the design or evalution of a monitoring program such as measurement error, minimum detection limits, quality assurance, or the determination of just how much precision is needed. Nevertheless the results and examples presented should provide some useful information on the design and evaluation of monitoring programs.

It should also be noted that the determination of monitoring objectives, the development and understanding of alternative monitoring methods, and the design of programs to meet these objectives are evolving in concert through ongoing activities. Specifically, several state and local agencies are currently monitoring noncriteria air pollutants, and the U.S. Environmental Protection Agency has a pilot phase of the Toxic Air Monitoring System (TAMS) underway.

MONITORING PROGRAMS

The Toxic Air Monitoring System (TAMS)

The U.S. Environmental Protection Agency (EPA) is currently developing a Toxic Air Monitoring System (TAMS), a network of stations to monitor up to 60 noncriteria air pollutants. One important goal of the TAMS is to enable researchers to assess long-term exposures to toxic air pollutants, hence our emphasis on the estimation of annual average concentrations.

An important limitation of the monitoring program is that precipitation interferes with the measurement of certain volatile organic compounds (VOC's) collected on Tenax adsorbent material. Lumpkin and Bond (1984) state that samples of this type taken during precipitation should not be used, however other monitoring methods less vulnerable to precipitation are under study.

Another important aspect of the monitoring program is that samplers must be operated at different flow rates and for different sampling periods to effectively monitor different compounds. For some VOC's the usual 24-hour integrated samples are not possible because the 24-hour air volume would exceed the retention volume (Walling, 1984). Thus, shorter sampling periods, e.g., 12-hour or 6-hour integrated samples, may be required. This adds the dimension of time of day to the design of the monitoring program.

The EPA plans to conduct a pilot monitoring program in a few urban areas (beginning with Boston, Chicago, and Houston) before the national network is established. The current sampling plan for the TAMS pilot network is to monitor at each site (1) certain volatile organic compounds (VOC's) collected on Tenax, (2) formaldehyde, (3) benzo(a)pyrene (BaP), and (4) the trace metals arsenic, cadmium, chromium, and nickel. Twelve-hour or 6-hour integrated samples of VOCs will be taken. Either 12- or 24-hour integrated samples of formaldehyde will be taken, and 24-hour integrated samples of BaP and the metals will be taken using high-volume ("hi-vol") particulate samples. The experience and data gained from the pilot program will enable the EPA to conduct the larger effort with greater efficiency.

Toxic Air Monitoring by State and Local Agencies

In addition to the planned national system for monitoring noncriteria air pollutants, many state and local agencies have or are planning programs to monitor these pollutants. A practical limitation of these programs, shared by national programs, is that only a proportion of the scheduled samples yield valid observations. Planned observations may be missed or invalidated because of precipitation or equipment failure, for example. The proportion of valid observations is known as the data capture rate.

ISSUES

A number of issues related to the TAMS are discussed by Thrall, Burton, and Moezzi (1984). These issues include the estimation of diurnal or seasonal components of variation, trade-offs between infrequent monitoring at several sites versus more frequent monitoring at one site, and the precision required of estimated annual concentrations given the uncertainty of our knowledge of the health risks associated with different pollutants.

In addition to the issues arising in national monitoring programs, a state or local agency may face the issue of determining whether the annual average concentration of a noncriteria pollutant is sufficiently high at some particular site to be of concern. If the concentration at which chronic human health effects occur is known, then the agency may wish to monitor the pollutant with sufficient frequency so that reliable comparisons can be made between the estimated annual average concentration and the specified annual mean level of concern. When the concentration at which chronic health effects occur cannot be specified, the agency may nevertheless wish to compare estimated annual averages to levels observed at other sites or during previous years so that sites requiring more intensive investigation can be identified.

Another issue is the monitoring frequency required to produce estimated annual averages of specified reliability. In this case, the agency's concern would be the more general one of obtaining data (i.e., estimated averages) of good quality. The two issues we discuss may be summarized as follows.

Reliability of Comparisons: What frequency of monitoring is required to produce reliable comparisons between the estimated annual average concentration and some specified level?

Reliability of Estimates: What frequency of monitoring is required to produce reliable estimates of the average of ambient concentrations over the entire course of the year, i.e., the average that would be obtained from an uninterrupted data record?

SOURCES OF INFORMATION

The TAMS network will provide needed information about the level and variability of noncriteria air pollutants. Although profiles of these pollutants have been compiled (see, e.g., Hunt, Faoro, and Duggan, 1984; Koch et al., 1984; and Singh et al., 1977, 1979, 1983), long-term records of ambient concentrations are rare. Our recommendations and examples are based on one of the few such long-term records. The California Air Resources Board (CARB) monitored trichloroethylene, carbon tetrachloride, and chloroform in El Monte from November 1982 through September 1983 and in three other sites in the Los Angeles area from January through September 1983. The data collected by the CARB are discussed by Hunt (1984) and by Thrall, Burton, and Moezzi (1984) and are summarized here in Table 1.

The concentrations reported in Table 1 represent 24-hour integrated samples. The data include 14 instances in which concentrations were below the lower detection limit of the monitoring instrument but were reported as equalling the instrument's lower limit. The data also include some suprisingly high concentrations, notably a 3 ppb concentration of chloroform recorded in downtown Los Angeles on 29 March 1983. These reported concentrations have been confirmed by both EPA and CARB technical staff, that is, the concentrations do not appear to be the result of transcription errors or faulty chemical analysis. For the time being we interpret these concentrations as indicative of occasionally high values at these sites, although the possibility remains that they are the result of either some gross error in the measurement process or some very unusual event.

THE PRECISION RESULTING FROM COMBINATIONS OF SAMPLING AND POLLUTANT CHARACTERISTICS

The bias and imprecision of estimated annual average concentrations serve as criteria to assess the need for more or less frequent monitoring of VOC's and other noncriteria air pollutants. Within the resources available, it is also important to accurately estimate variances, that is, to get some indication of the geographic variability of annual average concentrations within an urban area, and to obtain reliable estimates of the extremes and standard deviation of concentrations at a site over the course of a year, particularly during the initial operation of a network.

We emphasize, however, that we are restricting attention to the statistical reliability of estimated annual average concentrations, as mentioned in the introduction. That is, there are other important issues beyond the scope of the present discussion, such as the comparative costs of implementing various monitoring strategies, alternative monitoring objectives

TABLE	1.	Summar	ry stati	stics	for	three	volat	tile	organic	compounds	(VOCs) monitore	d at 1	four
sites	in 1	the Los	Angeles	Area	from	Novem	ber 1	1982	through	September	1983	(concentra	tions	are
expres	ised	in part	ts per b	illior).									

				Site		•
			Downtown			
Pollutant	Statistic	El Monte	Los Angeles	Dominquez	Riverside	Combined
Trichloroethylene	Average	0.289	0.565	0.283	0.327	0.331
	Standard Dev.	0.230	0.295	0.158	0.185	0.245
	Coefficient of Var.	0.796	0.522	0.560	0.566	0.739
	Maximum	1.200	1.500	0.680	0.870	1.500
	Minimum	0.020	0.020	0.100	0.020	0.020
	Sample Size	180	42	43	37	302
Carbon	Average	0.039	0.037	0.041	0.036	0.038
Tetrachloride	Standard Dev.	0.009	0.008	0.012	0.007	0.009
	Coefficient of Var.	0.242	0.224	0.297	0.193	0.247
	Maximum	0.073	0.060	0.080	0.060	0.080
	Minimum	0.010	0.010	0.030	0.030	0.010
	Sample Size	179	41	43	36	299
Chloroform	Average	0.062	0.144	0.051	0.061	0.072
	Standard Dev.	0.096	0.454	0.024	0.061	0.187
	Coefficient of Var.	1.542	3.148	0.471	1.007	2.611
	Maximum	1.100	3.000	0.140	0.400	3.000
	Minimum	0.020	0.020	0.020	0.020	0.020
	Sample Size	179	42	42	37	300

(e.g., comparing the influence on air quality of different sources of pollutant emissions, or estimating peak concentrations), or the public health benefits of the information to be gained from monitoring.

The trade-off between precision and sampling frequency is illustrated in Table 2 for sampling frequencies of 1/3, 1/6, 1/12. The table gives 95 percent confidence bounds on the magnitude of the error of the estimated annual average expressed as a percentage of the actual annual average (i.e., the relative difference, expressed as a percentage, between the estimated and actual averages). These bounds have been obtained from a normal distribution that approximates the sampling distribution of the estimated annual average concentration for a data capture rate (percentage of scheduled observations yielding valid data) ranging from 50 to 100 percent, and for a coefficient of variation (the standard deviation divided by the average, thus the relative variation about the average) ranging from 25 to 300 percent.

Table 2 shows, for example, that monitoring carbon tetrachloride at one of the four sites in the Los Angeles area with a 100 percent data capture rate will result in a relative error likely to be no more than 4 percent if 24-hour concentrations (or two consecutive 12-hour concentrations) are monitored once every three days. The bound changes from 4 percent to 9 percent if monitoring is scheduled once every 12 days. At the other end of the scale, monitoring chloroform in downtown Los Angeles with only a 50 percent data capture rate could result in a 69 percent error if monitoring were scheduled every three days.

Note that the table also provides precision bounds for monitoring 12-hour concentrations alternately during the night and day. One can, of course, effectively construct 24-hour observations by sampling during consecutive 12-hour periods. Alternatively, monitoring 24-hour concentrations once every 3, 6, or 12 days corresponds to monitoring 12-hour concentrations once every 36 hours, three days, or six days, respectively.

Similarly, the table can be interpreted for 6-hour samples. Again, 24hour averages can be formed if four consecutive 6-hour samples are taken at a time. The table then applies to blocks of 4 consecutive samples taken once every 3, 6, or 12 days. More generally, the table applies to sampling schedules that call for monitoring a representative one-third, one-sixth, or one-twelfth of the total number of possible sampling periods.

An important assumption used in the construction of the table is that the probability of data capture is independent of the probability of the occurrence of either high or low concentrations. Entries in the table

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TABLE 2. Ninety-five percent confidence bounds on the magnitude of the error of the annual average concentration estimated from scheduled monitoring of 24-hour concentrations once every three, six, or 12 days, respectively, when the error is expressed as a percentage of the actual annual average concentration.

Data Capture	Sampling		Coeffic	ient of	Variat	ion (%)	
Rate (%)	Frequency	25 ^a	50	75 ^b	100	200	300 ^C
	1/3	4	7	11	15	29	44
100	1/6	6	11	17	23	46	69
200	1/12	9	17	26	34	68	102
	1/3	4	8	12	16	31	47
90	1/6	6	12	18	24	49	73
	1/12	9	18	27	36	72	108
	1/3	4	9	13	17	34	51
80	1/6	7	13	20	26	52	78
	1/12	10	19	29	38	77	115
	1/3	5	9	14	19	37	56
70	1/6	7	14	21	28	56	85
	1/12	10	21	31	41	82	124
	1/3	5	10	15	21	41	62
6 0	1/6	8	15	23	31	62	92
	1/12	11	22	34	45	89	134
50	1/3	6	11	17	23	46	69
	1/6	9	17	26	34	68	102
•	1/12	12	25	37	49	98	148

^a 25 percent corresponds roughly to the combined CV for carbon tetrachloride in Table 1.

^b 75 percent corresponds roughly to the combined CV for trichloroethylene in Table 1.

^C 300 percent corresponds roughly to the combined CV for chloroform in Table 1.

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would have to be modified if it were known, for example, that daytime concentrations tended to be higher or lower than nighttime concentrations and that a disproportionate number of, say, nighttime observations would fail to yield valid data.

From the table we see that for a pollutant and site for which the coefficient of variation and data capture rate are known, or can be estimated, precision increases roughly in proportion to the square of the expected number of valid observations. For example, the error bound for samples taken once every 12 days is roughly twice that for samples taken once every three days.

In designing a network consideration must be given to: (1) the expected data capture rate (including loss of samples due to precipitation); (2) the likely coefficients of variation of different pollutants at different sites; and (3) the desired bounds on the percentage error of estimated annual average concentrations. Thrall, Burton, and Moezzi (1984) discuss these and other considerations in their review of the CARB data.

EXAMPLES OF TRADE-OFFS BETWEEN PRECISION AND SAMPLING FREQUENCY

In choosing a monitoring frequency, one should consider not only the desired level of precision, but also the likely data capture rate (the proportion of scheduled monitoring days that yield valid observations), and the number and types of sources of pollutant emissions that would influence the level and variability of ambient concentrations from day to day. The following examples illustrate this point.

Example 1. Suppose that the annual average concentration of trichloroethylene at a new monitoring site is to be compared to the approximately 0.3 ppb recorded at three of the four sites located in the Los Angeles area listed in Table 1. Suppose also that we are willing to assume that the daily ambient concentrations at the new site are not much more variable than those at the Los Angeles sites, i.e., that the coefficient of variation (the standard deviation expressed as a percentage of the annual average) at the new site is 100 percent (the maximum coefficient of variation among the four Los Angeles sites is about 80 percent), and that the likely data capture rate will be 75 percent.

Finally, we want to be confident that the estimated average concentration will fall below 0.3 ppb if the actual value is below 0.3 ppb, and, conversely, that the estimate will fall above 0.3 ppb if the actual average is above 0.3 ppb. Of course, if the actual average concentration equals

0.3 ppb or is very close to this level, the estimate may easily fall above or below the 0.3 ppb level. So, to be more precise, we may require sufficiently frequent monitoring such that, say, with 90 percent probability, the estimate will fall on the same side of the 0.3 ppb level as the actual average, provided that the magnitude of the relative difference between the specified 0.3 ppb level and the actual annual average concentration at the site is at least 10 percent. Under these circumstances the required frequency of scheduled monitoring is about once every three days. The derivation of the required monitoring frequency will be explained shortly.

<u>Example 2</u>. Suppose now that we plan to compare the annual average concentration of chloroform to be obtained at the new site with the approximately 0.06 ppb obtained at the same three Los Angeles sites as in Example 1. Suppose, again, that the data capture rate is 75 percent, and that we want to be 90 percent confident of a correct comparison, provided that the magnitude of the relative difference between the specified 0.06 ppb level and the actual average concentration is at least 10 percent. The required sampling frequency now depends on whether the relative variability, i.e., the coefficient of variation, of daily ambient concentrations at the new site resembles that of Riverside or that of downtown Los Angeles. A site resembling Riverside would have a coefficient of variation of about 100 percent, and the required sampling downtown Los Angeles would have a coefficient of variation of about 300 percent, and everyday sampling would be required.

The required frequency can be formulated as follows. If we let f denote the frequency of scheduled monitoring, then f^{-1} is the period between scheduled samples, so that monitoring is scheduled "once every f^{-1} days" (or, more generally, once every f^{-1} time intervals). In Examples 1 and 2, f^{-1} was obtained using the following formula (derived in the appendix):

$$f^{-1} = p \cdot \left(1 + \frac{N \cdot r_L^2}{c v^2 \cdot z^2} \right)$$
(1)

where

p = the proportion of scheduled monitoring days that yield valid observations, also known as the data capture rate; in our exampes p = 0.75;

^{*} The "relative difference" between two numbers, x and y, is (x - y)/y.

- N = the total number of time intervals in a year, e.g., N = 365 in our examples, corresponding to the number of 24-hour intervals in a year;
- rL = a lower limit on the magnitude of the relative difference between the specified level and the new site's actual annual average concentration; r = 0.1 in our examples; corresponding to our objective of identifying differences as great or greater than 10 percent;
- CV = the coefficient of variation (the ratio of the standard deviation divided by the average) at the new site, e.g., 1.0 to 3.0 in our examples;
- z = the percentile of the standard normal distribution, corresponding to the level of confidence desired for a correct comparison; in our examples z = 1.282, corresponding to the desired 90 percent level of confidence; in general, setting z equal to the (1α) th quantile produces a (1α) level of confidence, 90 or 95 percent being typical choices in statistical applications.

Generally, Equation 1 should be regarded as providing an initial approximation to the required monitoring frequency. If the number of valid observations per year $(f \cdot p \cdot N)$ is less than 20, then it is advisable to override Equation 1 with the recommendation of Hunt, Faoro, and Duggan (1984) that at least five valid observations per quarter be obtained. Similarly, it is wise to avoid monitoring exclusively on one day of the week, even if such a schedule is obtained from Equation 1, because pollutant levels may differ substantially on different days of the week. Finally, a once-per-six-day monitoring schedule is common among many agencies, and it may be practically important to coordinate the new schedule with existing schedules. Since Equation 1 approximates the minimum amount of monitoring needed to meet specified criteria, any adjustments to the derived sampling frequency should generally be in the direction of providing more frequent monitoring. The next examples illustrate these suggestions.

Example 3. Suppose that the annual average concentration of carbon tetrachloride at the new monitoring site is to be compared to the approximate 0.04 ppb obtained at the four sites in the Los Angeles area listed in Table 1. Suppose, again, that the expected data capture rate is 75 percent (p = 0.75), and that we want to be 90 percent confident of a correct comparison (z = 1.282, the 90th percentile of the standard normal distribution) if the magnitude of the relative difference between the specified 0.04 ppb level and the new site's actual average concentration is at least

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10 percent ($r_L = 0.1$). Finally, let us assume that the coefficient of variation for the new site is only 25 percent (CV = 0.25), which is the approximate value at the Los Angeles sites.

Due to the low coefficient of variation, Equation 1 yields an approximate once-per-34-days sampling schedule $(f^{-1} = 34)$, i.e., about 11 scheduled monitoring days per year, which, using the 75 percent data capture rate, can be expected to yield about eight valid observations per year $(f \cdot p \cdot N = 8)$. Since this is less than the recommended 20 valid observations per year, we would adopt the suggestion of Hunt, Faoro, and Duggan (1984) that at least five valid observations per quarter be obtained. Based on the 75 percent data capture rate, we might therefore schedule monitoring once every 12 days. (A straightforward calculation yields a sampling schedule of once every 13.7 days; monitoring every 12 days thus allows for a data capture rate in one or more quarters that is somewhat less than 75 percent.)

When we have no specific concentration to which the calculated annual average is to be compared, we may simply require that the average obtained from intermittent monitoring be close to the average of ambient concentrations over the entire course of the year.

One way to express this requirement is that the relative difference between the calculated and underlying annual averages should be, say, less than 10 percent with at least 90 percent probability. Equation 2 (derived in the appendix) provides a formula for calculating the sampling period, f^{-1} , meeting these requirements:

$$f^{-1} = p \cdot \left(1 + \frac{N \cdot r_U^2}{CV^2 \cdot z_2^2} \right)$$
(2)

where r_U is the desired upper limit (e.g., 0.1) on the magnitude of the relative difference, z_2 is the percentile of the standard normal distribution corresponding to the desired confidence level,* and N, p, and CV are as given under Equation 1. Again, Equations 1 and 2 merely provide an initial approximation to the required monitoring frequency (see the remarks following Equation 1).

^{*} To achieve the confidence level $1 - \alpha$, z_2 should be the $1 - (\alpha/2)$ quantile of the standard normal distribution, e.g., z_2 should be the 95th percentile (1.645) to achieve 90 percent confidence.

Example 4. Suppose that a state or local agency plans to monitor 24-hour concentrations of carbon tetrachloride sufficiently often so that the relative difference between the estimated and actual annual average concentrations will be no more than 10 percent with 90 percent probability $(r_U = 0.1, z_2 = 1.645)$. The coefficient of variation is assumed to be 25 percent (CV = 0.25), consistent with the data from Table 1, and the data capture rate is assumed to be 75 percent (p = 0.75). Since there are 365 24-hour intervals in the year (N = 365), Equation 2 yields an approximate sampling schedule of once every 17 days ($f^{-1} = 17$). However, since the expected number of valid observations is less than 20 (f•p•N is approximately 16), a schedule of once every 12 days would be more appropriate, consistent with the remarks in example 3.

Example 5. Suppose that the situtation is as described in example 4, except that the measurement method is based on 12-hour samples rather than 24-hour samples. Application of the formula for the required sampling frequency now indicates monitoring one out of every seventeen 12-hour intervals. This could be achieved in a number of ways, e.g., monitoring for 12 hours every 8 1/2 days (thus alternating between nighttime and daytime monitoring) or monitoring during two consecutive 12-hour intervals every 17 days. There may be some statistical advantage to one scheme over the other, depending on the pattern of daytime and nighttime concentrations. Also, in order to match other monitoring schedules, it may be more convenient to take alternate nighttime and daytime samples once every six days, or to take two consecutive samples once every twelve days. In any case, if the annual average is to be estimated as the simple arithmetic average of all valid 12-hour samples collected during the year, it is important to obtain about the same number of nighttime and daytime samples to avoid biasing the estimated annual average.

Example 6. Again, let us suppose that the situation is as described in example 4, this time with 6-hour samples. Equation 2 now indicates monitoring one out of every seventeen 6-hour intervals. This might be accomplished most conveniently by monitoring four consecutive 6-hour intervals once every 17 days. This frequency might be increased to monitoring four consecutive 6-hour intervals once every 12 days to better coincide with other monitoring schedules. Other sampling designs are possible, but if the annual average is to be estimated as the simple arithmetic average of all valid 6-hour samples collected during the year, it is important to obtain approximately the same number of valid observations for each 6-hour interval of the day.

SUMMARY

The development of a program to monitor specified noncriteria air pollutants is a large undertaking with many potential objectives, constraints, and unknowns. This guideline focuses on the monitoring frequency needed to reduce to a specified level the effect of sampling error on the estimated annual average concentration of a pollutant at one monitoring station. "Sampling error" here refers to the fact that the annual average must be estimated from a sample of say, days in the year, since practical constraints limit how often monitoring can be scheduled. In principle the problem of sampling error may be eliminated by monitoring every day or, more generally, during every possible time interval (practically, however, missing or invalid observations can and do occur in this case as well). Thus the guideline addresses one aspect, solvable at least in principle, of a larger and more difficult problem.

Within the sampling error context, a formula is derived in the appendix for the probable error in the estimated annual average as a function of monitoring frequency, data capture rate, and the relative variation of pollutant concentrations over the course of the year. The formula is illustrated in Table 2 and the concluding examples show how related formulas can be used to determine the monitoring frequency needed to limit the probable error to a prescribed magnitude. In some cases where the relative variation in pollutant concentrations is low, the derived infrequent monitoring is overridden by a longstanding EPA recommendation that at least 5 valid observations per quarter be obtained.

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Appendix

DERIVATION OF THE RELATIONSHIP BETWEEN SAMPLING FREQUENCY AND THE PRECISION OF THE ESTIMATED ANNUAL AVERAGE CONCENTRATION

We would like to know the annual average concentration, μ of a pollutant based on a complete set of N measurements. The number of possible observations to be obtained from the schedule of intermittent monitoring is some fraction (f) of N, and only a proportion, p (the so-called "data capture rate") of the scheduled monitoring intervals will produce valid observations. That is, environmental conditions may prohibit scheduled monitoring in some instances; in other cases some mishap in the data collection process may invalidate observations or cause them to be missed. So from a total of N possible measurements we obtain only pfN valid observations, which we regard as a random sample from a finite population.

Letting $\widehat{\mu}$ denote the sample average concentration, the expected value and variance of $\widehat{\mu}$ are

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$$E\mu = \mu$$

$$Var \hat{\mu} = \frac{1 - fp}{fp} \frac{\sigma^2}{N}$$

where σ^2 is the population variance of the N measurements. Moreoever, if the number of valid and missing (or invalid) measurements is large, i.e., if both pfN and N - pfN are large, and if there are relatively few exteme concentrations, then the sampling distribution of $\hat{\mu}$ is approximately normal. (The conditions for asymptotic normality are formulated more precisely by Cochran, 1963, who cites Hajek, 1960.)

The approximate normality of $\hat{\mu}$ may be conveniently expressed as the approximate normality of the relative error of $\hat{\mu}$:

$$\frac{\hat{\mu} - \mu}{\mu} \sim N(0, \tau_N^2)$$

where

$$\tau_{\rm N}^2 = \frac{1 - fp}{fp} \frac{{\rm CV}^2}{{\rm N}}$$

 $CV = \frac{\sigma}{u}$ is the coefficient variation.

We can use these results to obtain approximate answers to the following two problems.

<u>Problem 1</u>. How frequently should monitoring be scheduled in order to limit the probability of an erroneous comparison of $\hat{\mu}$ to a specified concentration μ_0 , i.e., of obtaining $\hat{\mu} > \mu_0$ when $\mu < \mu_0$ or vice versa?

<u>Problem 2</u>. How frequently should monitoring be scheduled to limit the relative error of $\hat{\mu}$ to a prescribed level?

We formulate problem 1 as follows. Since the chance of an erroneous comparison is large if μ is close to μ_0 , we suppose that the magnitude of the relative difference between μ_0 and μ is not less than some prescribed lower bound, r_i :

$$\left|\frac{\mu_0 - \mu}{\mu}\right| > r_L.$$

We want the probability of an erroneous comparison to be no more than some prescibed value, say α . Thus, if $\mu > \mu_0$, we require that

 $\alpha > \Pr(\hat{\mu} < \mu_0)$ $> \Pr\left(\frac{\hat{\mu} - \mu}{\mu} < \frac{\mu_0 - \mu}{\mu}\right) \quad .$

Since the magnitude of the relative difference between μ_0 and μ may be as small as r_1 , this implies

$$\alpha > \Pr\left(\frac{\hat{\mu} - \mu}{\mu} < -r_{L}\right)$$
$$= \Phi\left(-r_{L}/\tau_{N}\right)$$

where Φ is the standard normal cumulative distibution function.

Or, if $\mu < \mu_0$, we require that

$$\alpha > \Pr(\hat{\mu} > \mu_0)$$
$$= \Pr\left(\frac{\hat{\mu} - \mu}{\mu} > \frac{\mu_0 - \mu}{\mu}\right)$$

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This implies that

$$\alpha > \Pr \quad \frac{\mu - \mu}{\mu} > r_{L}$$
$$= 1 - \phi(r_{L}/\tau_{N})$$

= $\Phi(-r_{\rm L}/\tau_{\rm N})$ from the symmetry of the normal distribution.

Thus, in either case, we require that

$$\alpha \geq \Phi(-r_L/\tau_N)$$
,

or

$$1 - \alpha \leq \Phi(r_L/\tau_N)$$
 ,

so that

$$\tau_N^2 \leq r_L^2/Z_{1-\alpha}^2$$
,

and hence,

$$\frac{1}{f} < p\left(1 + \frac{N \cdot r_{L}^{2}}{cv^{2} \cdot z_{1-\alpha}^{2}}\right) \qquad (1)$$

Here $Z_{1-\alpha}$ denotes the $(1-\alpha)th$ quantile of the standard normal distribution.

Problem 2 can be treated similarly. We want the magnitude of the relative error of $\hat{\mu}$ to be no more than some upper bound, say r_U , with a high probability, say 1 - α . We thus have

$$1 - \alpha \leq \Pr\left(-r_{U} \leq \frac{\hat{\mu} - \mu}{\mu} \leq r_{U}\right)$$
$$= \Phi(r_{U}/\tau_{N}) - \Phi(-r_{U}/\tau_{N})$$
$$= 2\Phi(r_{U}/\tau_{N}) - 1 .$$

Thus

$$1 - \alpha/2 \leq \Phi(r_U/\tau_N)$$
,

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or

$$Z_{1-\alpha/2} < r_U/\tau_N$$
,

so that

$$\tau_N^2 < r_U^2 / Z_{1-\alpha/2}^2$$
,

and hence

$$\frac{1}{f} < p\left(1 + \frac{N \cdot r_{U}^{2}}{cv^{2} \cdot z_{1-\alpha/2}^{2}}\right) \qquad (2)$$

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