United States Environmental Protection Agency Industrial Environmental Research Laboratory Cincinnati OH 45268

Research and Development

EPA-600/S2-80-186 Dec 1980



Project Summary

Evaluation and Application of SO_x Measurement Procedures for Kraft Recovery Furnaces

A. K. Jain, R. O. Blosser, D. B. Newport, and H. S. Oglesby

A research program was initiated to determine sulfuric acid (\$O₃/H₂SO₄) and sulfur dioxide (\$O₂) emissions from kraft recovery furnaces using an extractive sampling system. The Goksoyr and Ross controlled condensation technique, which uses a modified Grahm condenser, was chosen because of its reported accuracy. Equipment was designed and fabricated to evaluate the effect of coil length, frit porosity, temperature, flow rate, and concentration on the efficiency of H₂SO₄ capture.

Laboratory tests were conducted to determine the optimum design and operating conditions to minimize SO₃/H₂SO₄ losses in filter holders used in the sampling train for particulate separation. The effects of recovery furnace particulate on SO₃/H₂SO₄ losses were investigated. The alkaline particulate from the recovery furnace reacted with a part of SO₃/H₂SO₄ in the sample. Although the losses could not be correlated with the alkalinity of the particulate, they were not considered significant.

Field studies were conducted on five representative kraft recovery furnaces to determine SO₃/H₂SO₄ and SO₂ concentrations in flue gases. The SO₃/H₂SO₄ concentrations varied from 0 to 2.98 ppm, and the range of SO₂ concentrations varied from 14 to 416 ppm. A comparison of these emissions with the SO₃/H₂SO₄ and SO₂ emissions from oil- and coal-

fired utility boilers shows the kraft recovery furnace emissions to be much lower.

Introduction

Because of their adverse effect on respiratory functions, acid sulfate aerosols in the ambient air are of special concern in air quality management programs. One of the precursors of ambient acid sulfate aerosols is sulfur trioxide (SO₃), which is formed during the combustion of sulfur containing fossil fuels.

In the kraft pulping industry, the concentrated spent cooking liquor (black liquor), which consists of wood components, inorganic chemicals, and sulfur compounds, is sprayed into a furnace and combusted. Although the kraft recovery furnace burns black liquor in a manner to minimize sulfur dioxide (SO₂) generation, the presence of high concentrations of sulfur in the black liquor has raised the question of the possible presence of sulfur trioxide (SO₃)/sulfuric acid (H₂SO₄) in kraft recovery furnace flue gas

The objective of this investigation was to determine representative SO_2 and SO_3/H_2SO_4 levels in kraft recovery furnace emissions Sampling flue gases from the kraft recovery furnace is difficult because the flue gases are about 20 percent moisture and contain alkaline particulate which can react with SO_3/H_2SO_4 during sampling. The

investigation was divided into four areas:

- Development and laboratory testing of a suitable method to measure SO₃/H₂SO₄ concentration in a particulate-free gas stream.
- Determination of the effect of the presence of kraft recovery furnace particulate on the measurement of SO₃/H₂SO₄,
- 3 Selection and testing of a suitable particulate separation device to minimize particulate interaction with SO₃/H₂SO₄ in the sampling train if particulate is found to interfere in SO₃/H₂SO₄ measurement, and
- 4 Measurement of SO₂ and SO₃/H₂SO₄ levels in kraft recovery furnaces from five representative sources in the southeast

Conclusions

The kraft recovery furnace SO_x study results can be divided into two parts laboratory investigation and field measurements of SO_x emissions

Laboratory Investigation

A study of the Goksoyr and Ross method for SO_3/H_2SO_4 measurement showed that the efficiency of SO_3/H_2SO_4 capture in the modified Grahm condenser was dependent upon the frit porosity and coil length (Table 1) A condenser with Type C (Ace Glass) frit and a 200-cm coil maintained at 75° to 85°C (167-195°F) was the most suitable for use in the sampling train because of its ability to provide high H_2SO_4 capture efficiency and acceptable sampling rate in the range of 6-8 L/m

Tests to find a suitable filter holder for removing particulate from the gas stream prior to SO_3/H_2SO_4 measurement showed that the conventional EPA Method-5 type of filter holders could not withstand the desired temperature of $260^{\circ}C$ ($500^{\circ}F$) A quartz filter assembly, developed for another EPA project, was fabricated and tested in the laboratory. The study showed no significant loss of H_2SO_4 in the filter support assembly maintained above $260^{\circ}C$ ($500^{\circ}F$)

The effect of kraft recovery-furnace particulate upon the passage of SO_3/H_2SO_4 through the filter holder

 Table 1.
 Effect of Frit Porosity Upon SO₃ Condenser Efficiency.

No.	Frit Type*	Max. Pore Dia. Range (μM)	Length of Condensing Coil (cm)	Flow Rate (Lpm)	% H ₂ SO ₄ Capture
1	В	70-100	100	2	20-40
2	D	10-20	200	2	99
3	С	25-50	200	2-8	90-99

*Ace Glass

Table 2. H₂SO₄ Losses in Tests With Recovery Particulate

H₂SO₄ Conc	, H₂SO₄ Loss,		_	H₂SO₄ Loss* Possible		erence
ppm	ppm	Percen	nt ppm	Percent	ppm	Percent
20 0	3.4	17	1 4	7	2.0	10
23 0	60	26	16	7	4.4	19
28 8	4.3	15	14	5	2.9	10
32 3	0.3	1	10	3	-07	- 2
8.8	14	16	31	<i>35</i>	17	- 19
11 1	4 1	37	32	29	09	8
22 2	24	11	07	3	17	8
194	27	14	06	3	2.1	11
177	25	14	0.5	3	2.0	11

*If all alkalinity present was neutralized

was determined by continuously loading the quartz filter with recovery-furnace particulate while passing a gas stream containing H_2SO_4 through the filter. The results (Table 2) show substantially higher losses of H_2SO_4 than were expected based upon the alkalinity of the particulate and may be due to the adsorption of H_2SO_4 on the particulate surface. The absolute values of H_2SO_4 losses were, however, low and, for purposes of estimating emission levels from kraft recovery furnaces, of little significance

The alkaline particulate present in the kraft recovery furnace stack gas offered a potential for SO_3/H_2SO_4 loss from the sample. To minimize the contact between the gas and the collected particulate and to reduce the potential for SO_3/H_2SO_4 loss, tests were conducted with an electrostatic precipitator

obtained from the EPA Environmental Sciences Research Laboratory Tests showed that the precipitator removed 99 percent of the particulate present in a stack gas following a precipitator, and there was no conversion of SO_2 to SO_3 in the precipitator

Field Measurement of SO_x Emissions

The SO_x emissions from five kraft recovery furnaces were measured Included were two furnaces with direct contact evaporators (DCE) and three without any contact evaporators. One of the non-contact furnaces was a cross-recovery furnace in which 30 percent of the liquor was from the sodium-based semichemical cooking process.

The sampling train is shown in Figure 1 Table 3 summarizes test results by

furnace type and sample conditioning techniques. The data for all the tests show a SO_3/H_2SO_4 concentration range of 0 to 2 98 ppm, with an average value of 0.81 ppm. When separated according to the type of furnaces, the data show that DCE furnaces have an average SO_3/H_2SO_4 concentration of 0.24 ppm in stack gases; non-DCE furnaces have a slightly higher average concentration (1.07 ppm) Non-DCE furnaces had an average concentration of 356 ppm of flue gas SO_2 , substantially higher than the average concentration in furnaces with DCE (80 ppm)

The data in Table 3 indicate that non-DCE furnaces have an average SO_3/H_2SO_4 level of 0.90 ppm when a quartz filter was used in the sampling train, a lower average than the SO_3/H_2SO_4 concentration of 1.62 ppm obtained with a miniature electrostatic precipitator (ESP) in the sampling train

for particulate separation. These differences, too small to be of any importance, may be due to source variability, oxidation of SO_2 to SO_3 in the ESP during sampling, or lower losses of SO_3/H_2SO_4 in the ESP.

The lower SO₂ concentrations in DCE furnaces were anticipated and are generally due to SO₂ scrubbing in the DCE

To determine any linear correlation between the SO_3/H_2SO_4 and the SO_2 concentrations, the values of coefficient

Table 3. SO₃/H₂SO₄ Emission Data Summary

		SO ₃ /H ₂ SO ₄ Conc , ppm			SO ₂ Conc.,	
Samples	No.	Мах.	Mın	Avg	ppm	
All Samples	26	2 98	0	0.81	260	
Types of Furnaces						
-DCE Furnaces	9	1 10	0	0 24	80	
–non-DCE Furnaces	17	2 98	017	1 07	356	
Non-DCE Furnaces						
-Quartz Filter Only	13	2 63	0.17	0 90	430	
-ESP Only	4	2 98	0.91	1 62	305	

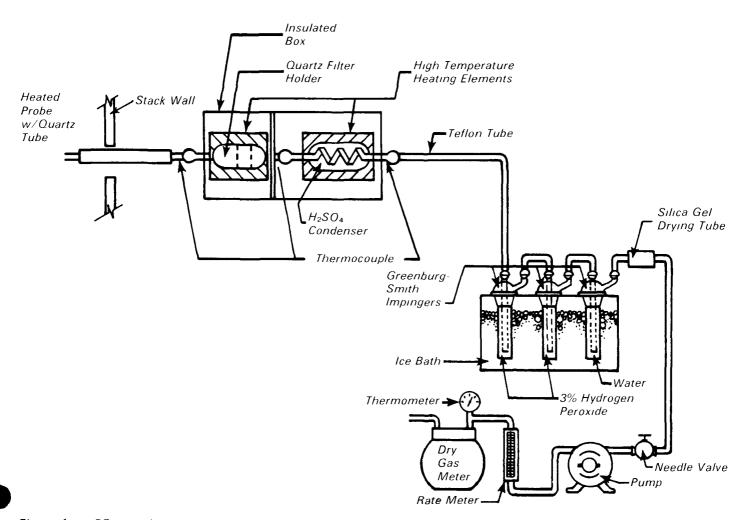


Figure 1. SO_x sampling train

of correlation (r) between SO_3/H_2SO_4 and SO_2 were determined for each recovery furnace and are tabulated in Table 4. These results, except for recovery furnace C, show a very poor correlation between SO_3/H_2SO_4 and SO_2 . If a high level of SO_2 is noted in a particular furnace's stack gas, it should not be assumed that the same furnace also emits a high concentration of SO_3/H_2SO_4 .

Table 4.Coefficient of Correlation SO_3/H_2SO_4 and SO_2 .

Recovery Furnace	Coefficient of Correlation
A	-0.33
В	-0.50
С	0 99
D	-0 42
E	-0 46

To understand the relative significance of the SO_x levels in kraft recovery furnace stack gases, these levels must be compared to emissions from oil- or coal-fired utility or industrial boilers. Some of the recently published SO_2 and H_2SO_4 emission data from oil- and coal-fired boilers show that both the SO_2 and the H_2SO_4 concentrations in flue gases from oil- and coal-fired boilers are much higher than the levels in kraft recovery furnace stack gases

A. K. Jain, R. O. Blosser, D. B. Newport, and H. S. Oglesby are with the National Council of the Paper Industry for Air and Stream Improvement, Inc., New York, NY 10016.

Michael D. Strutz is the EPA Project Officer (see below).

The complete report, entitled "Evaluation and Application of SOx Measurement Procedures for Kraft Recovery Furnaces," (Order No. PB 81-109092; Cost: \$7.00, subject to change) will be available from:

National Technical Information Service

5285 Port Royal Road Springfield, VA 22161

Telephone: 703-487-4650

The EPA Project Officer can be contacted at: Industrial Environmental Research Laboratory U.S. Environmental Protection Agency

Cincinnati, OH 45268

United States Environmental Protection Agency Center for Environmental Research Information Cincinnati OH 45268 Postage and Fees Paid Environmental Protection Agency EPA 335



Official Business Penalty for Private Use \$300

[