



Project Summary

Compatibility of Source Separation and Mixed-Waste Processing for Resource Recovery

Louis Soldano, Stephen C. James, and Charles Miller

This report evaluates whether source separation and mixed-waste processing of municipal solid waste are compatible approaches for recovery of materials and energy in the same community or region. Existing source separation programs and mixed-waste processing facilities were analyzed to develop typical options for assessment. Among the issues addressed are changes in production of useful energy from a mixed-waste processing facility; air and water pollution; residual solid waste; employment; operator profitability; total solid waste collection costs; and quantities of recycled materials.

This Project Summary was developed by EPA's Municipal Environmental Research Laboratory, Cincinnati, OH, to announce key findings of the research project which is fully documented in a separate report of the same title (see Project Report ordering information at back).

Introduction

Are source separation and mixed-waste processing (MWP) of municipal solid wastes compatible approaches for recovery of materials and energy in the same community or region? With source separation, salable materials (currently aluminum, ferrous metals,

paper, and glass) are segregated from wastes at the point of discard for collection and processing. With MWP, collected, mixed municipal wastes are centrally processed to convert the mixed wastes into energy and, if possible, to separate recyclable material. The basic difference between the two approaches is that source separation requires the separation of wastes by the householder whereas MWP relies on machinery.

Conflicts may arise between the two methods, however. Both may overlap in recovering a single material from the waste stream. Supporters of source separation claim to recover the highest economic value, operators of MWP facilities claim that separation of certain materials reduces the energy content of the solid waste and causes financial loss to plants that require a fixed amount of waste to break even. Mutual benefits can be seen where source separation allows a larger amount of waste to be processed and increases equipment life by reducing abrasive materials. Conflicts may be the result of poor coordination rather than inherent conflicts.

Procedure

Resource recovery was analyzed from the viewpoint of the mixed-waste plant operator, the municipality, and the

nation. For each viewpoint, specific issues that would be most important are identified—energy materials conservation, environmental impacts, economic impacts, and institutional/technical impacts. This assessment was conducted for a hypothetical community with solid waste data equal to national averages.

Scenarios were based on five source separation options: high-efficiency multi-material recovery, low-efficiency multi-material recovery, high-efficiency newsprint recovery, low-efficiency newsprint recovery, and beverage container recovery.

The following MWP alternatives and possible combinations were addressed: unprocessed combined waterwall combustion and ferrous recovery (UWCG); combined processed waterwall combustion and ferrous recovery (PWCF); refuse-derived fuel and ferrous recovery (RDFF), and modular incineration without ferrous recovery (MI). MWP facilities options were a fixed capacity plant, a variable-sized plant with a fixed service area, and a fixed capacity plant with an expandable service area.

The hypothetical community, Baselyn, has approximately 100,000 people in a major metropolitan area producing 200 tons of solid waste per day. The city's sanitation department collects solid waste from all households. There is a materials processor who buys newspaper for \$30/ton, corrugated paper for \$60/ton, high-grade paper for \$70/ton, and mixed glass and cans for \$10/ton.

For a "Fixed Service Area" of five communities like Baselyn producing 1,000 tons/day of waste, it may be economical to reduce plant size or collect waste from an outside area to make up for reduction in waste because of source separation. For "Variable Plant Size," it is assumed that the service area generates 1,000 tons/day of waste but alters the plant size to correspond to the waste remaining after source separation.

At present, the source separation programs discussed for Baselyn recover as much as 5 percent of the waste although as much as 10 percent can be recovered. The reason for this gap is that the waste generator has few incentives to recycle materials because the market prices fluctuate widely.

Six common methods of source separation are recycling centers, separation of office paper, separation of corrugated paper, separate collection of newsprint

and other paper, separate collection of various materials, and beverage container deposits.

Although the value to large commercial establishments of separating high-grade office paper varies, it does have good prospects for being economically feasible. Recovery rates for separated corrugated paper are high because of ease of physical separation and because recovery reduces mixed-waste collection costs to commercial establishments. Separate collection of newsprint and other paper depends on participating residents who place newsprint at the curbside in separate containers. Many of these programs have been well received. Separate collection of various materials is less common than single material programs because of the burden of separating and storing several different materials until collection day. Beverage container deposits, including mandatory deposit systems, place responsibility on the resident and can achieve recovery rates as high as 90 percent. Each of the above options, except recycling centers, was evaluated for Baselyn.

Source Separation Options

For *high-efficiency multi-material recovery*, ordinances required residents to separate their waste into mixed paper, clear glass and cans, mixed glass and cans, and remaining waste; scavenging of separated materials was prohibited. This option cost Baselyn \$982/day but provided revenues of \$546/day. Eliminating 35.1 tons of waste reduced landfill disposal costs from \$8,890 to \$7,330/day. If MWP was used, costs were reduced from \$7,770 to \$6,406/day. Baselyn was contractually required to supply the MWP operator with all remaining wastes.

This source separation program extended the 20-year life of the county's landfill by 3.6 years, lowered pollution emissions during the production process, and slowed resource depletion.

Low-efficiency multi-material recovery is similar to the case above except that participation is voluntary and there is no program for recovery of office or corrugated paper wastes. In this option, residents were asked to separate wastes into only three components—mixed papers, mixed bottles and cans, and remaining waste. The cost of the source separation program was \$513/day and revenues were

\$303/day. The source separation program reduced total disposal cost by \$394/day with landfill and by \$322/day with MWP. Because Baselyn had no ordinance to enforce source separation by residents, the city and intermediate processors were reluctant to enter into any long-term contract.

As in the first case, the county's landfill life was extended, but for only a little more than a year. This option had little effect on the groundwater pollution from the landfill and only small reductions in pollution emissions for MWP.

Two other options are *high- and low-efficiency newsprint recovery*—mandatory and voluntary. The mandatory program resulted in a 60 percent recovery; the voluntary program, 20 percent. The high-recovery program cost \$503/day with total revenues of \$270/day. Net disposal cost was reduced \$167/day for landfill and \$117/day for the MWP plant. In low recovery, there are revenues of \$90/day. In addition to the advantage of initial simplicity, the most important effect of these programs is a slight reduction in landfill requirements.

Beverage container recovery resulted from state legislation rather than local initiative. The program was operated by the private sector, and waste reduction was approximately 11.8 tons/day. This recovery provided a net energy of 102×10^9 joules/day. The mandatory deposit option would extend landfill life slightly but would greatly reduce roadside litter.

Mixed-Waste Processing Alternatives

MWP energy can be recovered as electricity, hot water or steam, or fuel. Inorganic materials usually recovered include ferrous metals, glass cullet, aluminum, and nonferrous metals. Organic materials recovered can be converted to compost, animal feed, or chemical industry feedstocks.

Unprocessed combined waterwall combustion and ferrous recovery (UWCF) consists of mass burning of collected mixed waste in a thick bed on a moving grate in a waterwall furnace. The ash is quenched before passing over a magnetic separator, where ferrous material is recovered and the residue is sent to a landfill.

Combined processed waterwall combustion and ferrous recovery (PWCF) is the same as UWCF except that the waste is shredded and sepa-

rated into light and heavy fractions. The light fraction, a higher quality fuel than combined waste, is burned. The heavy fraction is passed through a magnetic separator and the residue is sent to a landfill. More waste can be handled this way than in a UWCF.

Refuse-derived fuel production and ferrous recovery (RDFF) is similar to PWCF except that the light fraction is processed into a fuel than can be used on or off site.

Modular incinerators without ferrous recovery (MI) can be batch type or continuous feed type. Since the typical size is less than 50 tons/day, over 20 units would be required to handle 1,000 tons/day.

Areas of Concern

Energy

An analysis of the source separation options used in Baselyn showed that variations of the BTU content resulting from source separation to be small and well within the range of variation expected in raw municipal waste. For a fixed service area, source separation reduces both the percent and total amount of BTU recovery. For an expanded area, the total BTU recovery for each waste processing option is proportional to the BTU content/pound of the MWP stream.

Environmental Impacts

Environmental issues are emissions to air and water pollution from landfills. This analysis assumed that source separation and ferrous recovery were not contaminated. Calculations were based on 1,000 tons/day of mixed waste.

Although air emissions for each type of facility must be made on site-specific bases, emissions for each combination of options are reported. In general, particulate emissions were high enough to present potentially significant problems for all combined alternatives involving MWP facilities.

Residuals to landfills for each option were reported; the separation options extended the life of the landfill. Low newsprint option extended it 1.5 percent, and high multi-material separation extended it 17.6 percent. Greater extensions, up to 86.3 percent, can be attained by coupling source separation with MWP alternatives.

The magnitude of water pollution indicative of the amount of water discharged from the facility was reported. Source separation alone caused few changes in the major environmental problems of landfills, i.e., pollution of surface and groundwater resulting from leaching. MWP residuals created less leachate so that problem was greatly reduced.

Considering the pollution to air and water, no MWP alternative is clearly superior.

Economic Impacts

Typical contract provisions between operators of MWP plants and municipalities include long terms, guaranteed tonnages, guaranteed payment, established fees, and adjustments to fees. In considering the economics of MWP facilities, the quality and quantity of the source separation option will change revenues and cause higher costs per ton because of plant under-utilization. In the expanded service area, the only source separation scheme that has more than a minor effect on processing costs is the removal of beverage containers. Removing glass and metals reduces processing costs.

The effects of source separation and MWP are also considered in overall employment, railroad freight rates, influence on local decisions, savings on solid waste disposal costs, and reduction in fuel import needs.

Viewpoints

The Plant Operator's Viewpoint

The operator of a MWP facility has the objectives of receiving enough processable waste, recovering the cost of operation, marketing, and realizing a profit. The operator's concern with source separation is its effect on the quantity and quality of waste sent to the MWP plant.

For the operator, source separation offers both potential risks and benefits. Risks include reduction in supply of waste, lower profits, and difficulties in financing the plant. Potential benefits are lower maintenance costs when unwanted materials are removed and the possibility of securing additional quantities of waste for the plant. One problem with opening a MWP facility is that it may force local entrepreneurs to

lose their source of supply and cease operations. Source separation then becomes a part of the issue of "flow control," i.e., the ownership of wastes and the legal rights of political jurisdictions to specify where and how their wastes are disposed. MWP operators must address the issues of reliability of supply, profitability, cost of private financing, and whether source separation will inhibit recycled materials purchasers from committing themselves.

The Municipal Viewpoint

Municipal officials seek to dispose of the community's solid waste in the most economical and environmentally acceptable manner possible. The energy used in collecting and transporting source separated materials and remaining mixed wastes is a relatively small fraction of the energy available in the mixed waste. Use of source separation options reduces emissions from trucks and landfill requirements. Either source separation or MWP may require municipal actions with significant financial, legal, employment, tax, and political implications. The primary issue from the municipal standpoint is the effect of source separation on the economics of collection, transportation, and disposal of mixed solid waste.

The National Viewpoint

From the national viewpoint, interests in resource recovery include reducing fuel imports, conserving valuable material resources, and improving environmental quality. The national environmental issues are reduction of the amount of waste and provisions for proper solid waste disposal. Because landfill sites are becoming more difficult to obtain and the regulations governing them are becoming more stringent, any action reducing landfill requirements should be considered. Pollution occasioned by coal mining, processing, and transporting will be eliminated in situations where MWP energy recovery is substituted.

Conclusion

With proper planning, there is no inherent incompatibility in any combination of source separation options and MWP alternatives. As a matter of fact, analysis showed that combining any source separation option with any MWP

alternative will result in positive or neutral impacts. In all cases, combinations are available that result in a greater net benefit than implementing any one separately.

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*This Project Summary was authored by **Louis Saldano**, who is with the Municipal Environmental Research Laboratory, and **Stephen James** and **Charles Miller**, who are also the EPA Project Officers (see below).*

The complete report, entitled "Compatibility of Source Separation and Mixed-Waste Processing for Resource Recovery," was authored by M. G. Klett, W. H. Fischer, B. N. Murthy, H. H. Fiedler, L. M. Oliva, and R. Crystal. The above report (Order No. PB 81-213 480, Cost. \$15.50, subject to change) will be available only from:

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Project Summary

Modification of Optical Instrument for In-Stack Monitoring of Respirable Particle Size

A. L. Wertheimer

A light scattering instrument for *in-situ* measurements of particulates in the 0.2 to 20 micrometer diameter size range is described, and field test results are presented. The instrument is a modified version of a prototype built during a prior EPA contract, Number 68-02-2447. The upper limit of the size response has been extended from 10 to 20 micrometers, and several component and packaging changes have been incorporated to make the unit more suited to stack particulate survey applications. Low forward angle and 90° polarization dependent scattering is employed to make the measurements.

The completed instrument was tested at a coal-fired electric power generating facility. During the test a cascade impactor was used as a referee device and both instruments were run side by side in the outlet duct of the electrostatic precipitator.

The results show an excellent correlation between the two instruments with regard to the identification of a 1 μ m diameter peak in the particle size distribution. A second peak around 20 μ m was defined by the optical instrument, but could not conclusively be confirmed through the impactor data. The optical instrument handled well during the field test and was delivered to EPA for additional testing.

This Project Summary was developed by EPA's Environmental Sciences Research Laboratory, Research Triangle Park, NC, to announce key findings of the research project that is fully documented in a separate report of the same title (see Project Report ordering information at back).

Introduction

A prototype real-time *in-situ* monitor was developed and constructed on EPA Contract 68-02-2447 to measure particle size distribution of respirable particles in the 0.2 to 10 μ m range. The purpose of this project was to add a channel to cover the 15 μ m size range so as to include the upper cut-off of the inhalable particulate emissions from stationary sources.

The addition of the large particle channel required a series of changes in the optical and electronic assemblies of the original instrument. In the process of incorporating these changes, the latest available components were selected and packaging improvements were made, resulting in an instrument optimally suited for survey work and stack particulate analyses. The new instrument measures the size distribution in the 0.2 to 20 μ m range in five size fractions, using a low power helium neon laser light source.

The modified prototype instrument was tested at a coal-fired electric gen-

erating plant. Referee measurements were made with a cascade impactor. Both instruments reported a strong peak in particle size around one μm in diameter.

Procedure

Principles of Operation

The instrument was designed by using simple diffraction theory for the low angle forward scattered light, and rigorous Mie theory for the light scattered at 90° to the probe beam. By adding high angle scattering capabilities, the use of light scattering for particle analysis can be extended to the sub-micrometer size range.

The stack particulate monitor measures the light scattered by particles passing through a 2.5 cm by 36 cm slot at the end of a 152 cm (5 foot) long probe. The light source is a 2 milliwatt helium neon laser, which emits a coherent beam at 0.6328 μmeters . The scattered light signals are proportional to the volumes of particulate material present in each of five size fractions. Six scattered light readings are taken at precisely determined angles. The light signals are acquired through fiber optic cables and transmitted to detectors located in the transceiver. A digital microprocessor calculates a five channel, volume-by-size histogram, covering the size range from 0.2 μm to 20 μm .

Modification of the Prototype

Modification of the original instrument to add a 15 μm channel involved a number of significant changes. When appropriate, these changes were made so as to accommodate improvements suggested from field trial experience with the first unit. The pertinent aspects of the new design are discussed in the following paragraphs.

The xenon arc source was replaced by a low power (2 milliwatt) helium-neon laser, which provides better collimation of the source, and eliminates a troublesome electrical transient starting problem. A slightly larger collection lens system was designed to accommodate a wider range of forward scattering angles. However, the 90° collection system used in the earlier unit remains the same.

A beam alignment sensor was added to the tip of the probe to monitor any thermally induced shifts. Through ports accessible from the rear of the probe, the beam can be aligned in or out of the

stack by maximizing the reading on a meter adjacent to the adjustment ports.

A Z-80 microprocessor system replaced the original 8008 based electronics. The new system allowed for rapid and efficient implementation of the hardware and software changes required in modifying the unit. The new electronics is much more compact than the earlier version, and is combined with a small digital printer in a 20 pound transportable electronics console. A second, smaller box, contains the electronics power supply, packaged separately to avoid heat build-up on the control console box.

A summary of operational characteristics of the prototype is shown in Table 1. The measurement time can be set by the user and ranges from 5 seconds to 12 minutes. Immediately following the data collection, the size distribution is printed out at the console.

Calibration

The calibration process involved several steps and used a variety of materials. To properly fill the sample slot region under operating conditions simulating a flowing gas stream, an aerosol test chamber was constructed in the laboratory.

The major steps of the calibration process are outlined here.

- (1) During assembly, the light collecting apertures were checked for alignment and adjusted to insure that the correct angles were being measured
- (2) Di-octyl phthalate (DOP), a transparent liquid with an index of 1.49, was dispersed as a droplet suspension in the aerosol test chamber by a Phoenix Precision Aerosol Generator. This created a well-controlled size and loading of particles in the 0.2 to 3 μm size range. From the measured signal levels and knowledge of the loadings, detector gain adjustments were made to accommodate a uniform distribution of particles at 40 parts per billion.
- (3) The collection geometry and fiber transmission product at each angle was determined by measuring fresh, filtered cigarette smoke. Because the majority of the particulate volume is well below one μm in diameter, the forward scattering pattern does not change with particle size. A correction constant is thus defined for each

scattering angle, based on the difference between scattered light strengths observed and those predicted by theory.

Results

Laboratory Tests

As a check for consistency, the instrument was then used to measure the aerosol distributions employed to calibrate it. Figure 1 shows the filtered cigarette smoke distribution, indicating a large percentage of the material in the 0.3 μm size channel, while Figure 2 shows the measured and manufacturer's specifications for the DOP aerosol suspension. In both cases, agreement between expectation and observation is quite good.

To further check the performance and calibration, two other materials were run, burning red phosphorous, and solid glass spheres. The red phosphorous is used for tactical smoke screens, but no referee data was available. The instrument readings indicated roughly equal amounts of material in the 0.3 and 1.0 μm size channels. This is consistent with its intended tactical use since particles in this size range are the most efficient scatters per unit volume and thus provide good obstruction.

The solid glass spheres, from Potters Industries, Inc., were used to check performance of the larger size channels. The spheres are specified as "3 to 10 micron" size, but no additional data was provided or available. No material is reported in the 0.3 μm channel, as expected, and most of the material is in the 3.5 or 7.5 μm region. The material reported in the 15 μm channel may be caused by clumping of the beads due to electrostatic charges introduced in the suspension process. Microscopic examination of a bead sample collected during the test confirmed this, showing occasional clumping.

Field Test Performance

During July, 1980, the prototype instrument was tested at an east coast coal-fired electric power generating station. L&N personnel used the prototype instrument to measure particle size distribution in a duct leading to the smoke stack. Personnel from Northrop Services, Inc., Environmental Science (NSI-ES), participated in the tests, taking data with a cascade impactor, and provided the necessary data analysis

Table 1. Operational Characteristics of Stack Particulate Monitor

Size Range (Particle Diameter)	0.2 to 20.0 μm
Size Discrimination	Five volume fractions with centers at 0.3, 1.0, 3.5, 7.5, 15 μm
Mode of Operation	Low angle forward scattering and 90° polarization dependent scattering
Loading Range	0.01 to 1.0 grams of material/meter ³ (.023 to 2.3 grains/ft ³) or 4 to 400 parts/billion by volume (with s.g. of 2.5)
Measurement Time	Signal integration time selectable from 5 seconds to 12 minutes (including a 6-minute position)
Duct Velocity	1.5 to 18 meters/second (5-60 feet/second)
Duct Temperature	260° C maximum (500° F)
Instrument Temperature	2° C to 43° C (35 to 110° F)
Power Requirements	One 20A, 115 volt, 60 Hz outlet
<i>Physical Specifications</i>	
Probe Dimensions	152 cm long (60 inches) by 9 cm diameter (3 1/4 inches)
Sample Slot Dimensions	2.5 x 36 cm (1 x 14 inches)
Transceiver-Probe Assembly	203 x 25 x 25 cm, 31.8 kg (80 x 10 x 10 inches, 70 pounds)
Control Console	38 x 41 x 25 cm, 9.1 kg (15 x 16 x 10 inches, 20 pounds)
Electronics Power Supply	23 x 41 x 25 cm, 6.4 kg (9 x 16 x 10 inches, 14 pounds)
Blower	74 x 48 x 43 cm, 22.7 kg (29 x 19 x 17 inches, 50 pounds)
Probe Material	Type 316 Stainless Steel (except for optical components)

for that method. Six separate data sets were collected over two days. One set of data from each day is presented here.

All testing was performed at the outlet of the electrostatic precipitators and prior to the final exhaust fan. The testing section was a vertical flow duct, approximately 32 1/2 ft. wide by 7 ft. deep. Sampling ports are located horizontally across the wide side of the duct. Each port is a 6-inch diameter flanged pipe, approximately 14 in. long. Two adjacent ports were selected as test points. A summary of the stack conditions appears in Table 2.

All aerodynamic particulate sizing was performed using a University of Washington Mark III Cascade Impactor and necessary support equipment. Prior to actual source testing, all in-stack atmospheric measurements necessary for isokinetic and other calculations

were recorded. Velocity head and stack differential pressure measurements were performed using a type "S" pitot. In-stack temperatures were measured using a thermocouple system attached to the end of the pitot tube. Velocity profile measurements were made up to 4.5 ft. into the duct at both test ports, with the impactor sampling conducted at the point of both average velocity and close proximity to the optical instrument. The point used for sampling was approximately the mid-point of the duct or 4 ft. from the lip of the port flange.

The impactors were preheated to stack temperature before sampling to avoid moisture condensation within the impactor body. The duration of each test was varied according to the stack opacity, knowledge that this coal unit was within particulate emissions standards, and the visual inspection of the previous

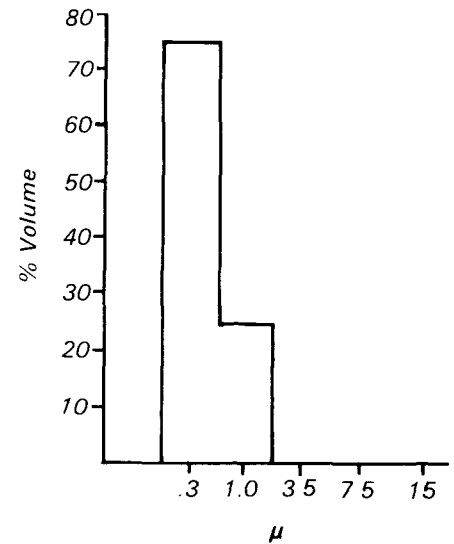


Figure 1. Calibration run using cigarette smoke

impactor test. Sample runs varied from 20 to 40 minutes in length.

Several hours were required to make the preliminary measurements before the impactors were inserted.

The prototype optical particle size monitor was prepared within approximately one hour. All electrical cables were connected and the instrument was turned on to warm-up the electronics. The optical alignment of the unit was adjusted using the external meter. The stack velocity, measured for the impactor runs, was used to set the purge flow rate on the blower. To facilitate insertion and removal from the stack during the tests, a suspension rail designed and built previously for this unit by NSI-ES was erected. A typical sample run lasted 6 minutes, and several runs were made during the impactor sample collection period.

On the first sampling day the boiler unit was operating at maximum output. On the second day, the boiler was operating at reduced output, and the particulate emissions were distinctly lower, dropping from around 0.02g/Nm³ the first day, to 0.007g/Nm³ the second, as measured by the impactor.

Results for both optical and inertial instruments are shown in Figures 3 and 4, plotted as histograms of volume fraction per unit log interval of particle-size. The optical data in each figure are indicated by the cross hatched histogram, while the impactor data are shown as the heavier outlined histogram. Variations in the individual channel widths

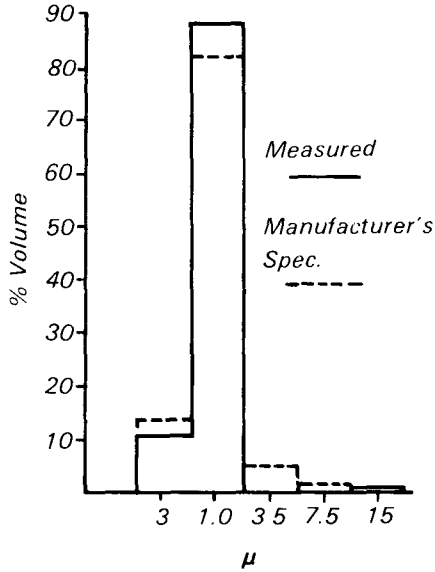


Figure 2. Calibration using dibutyl phthalate aerosol from Phoenix generator

are due to the different principles involved in measuring the particle distribution

The impactor data, provided by NSIES, were derived by plate weighings and computer assisted data reduction. A material density of 2.5g/cm^3 was assumed, and the channel edges were based on the aerodynamic separation properties of the individual stages of the impactor.

During each impactor run, continuous optical data measurements were made. The histograms shown are compiled from the time weighted average of the sequential optical data, which involved from 5 to 8 optical runs, depending on the length of the impactor run. The boundaries of the optical histogram are determined by the instrumental response, as calculated from scattering theory.

Discussion

The optical and inertial measurements agreed in some significant respects. In all runs both instruments reported a significant size fraction to be around one μm in diameter with, in most cases, substantial reductions in the amount of material above the one μm size. The optical instrument consistently indicated a good deal of material in its largest size channel, which made the distribution appear bimodal. This could not be definitely confirmed by the impactor data available, although impactor runs from some tests show a

Table 2. Stack Conditions During Field Test

Stack gas velocity:	45 to 50 feet/second
Stack gas temperature:	230 to 300° F
Gas pressure:	-2 inches of Hg
Direction of flow:	Vertical downward

leveling off of the distribution, and run 4 does indicate a secondary peak in its largest particle channel

The general agreement between the two methods is good. The size response question could well be resolved through further testing at other sites. There were some relatively minor technical problems, but none that should prevent the optical instrument from being used in other field tests. At the conclusion of this test, the prototype stack particulate monitor and its associated equipment were turned over to the EPA.

Conclusions and Recommendations

The primary goal of this work was to modify and test a prototype optical stack particulate monitor by the addition of a channel responding to particles in the $15\ \mu\text{m}$ size range. This was successfully accomplished. Tests in the laboratory showed results that agreed with expected size distributions of several

sample materials which were in the 0.2 to $20\ \mu\text{m}$ size range of the instrument. The field tests, conducted at a coal fired electric utility plant, provided size distribution data which were in excellent agreement with results reported by a referee inertial impactor. An additional advantage with the optical instrument is that size distribution data are computed and displayed immediately upon the conclusion of the signal collection sequence.

A secondary goal of this project was to improve the reliability and portability of the instrument to make it more suitable for stack survey work. The modified prototype unit is lighter and smaller than the original, and the operational improvements, such as ease of alignment and reliability of operation, were demonstrated during the field trial.

There may be some value in developing an on-site technique to provide the operator with a quick means of checking the calibration of the unit. Although

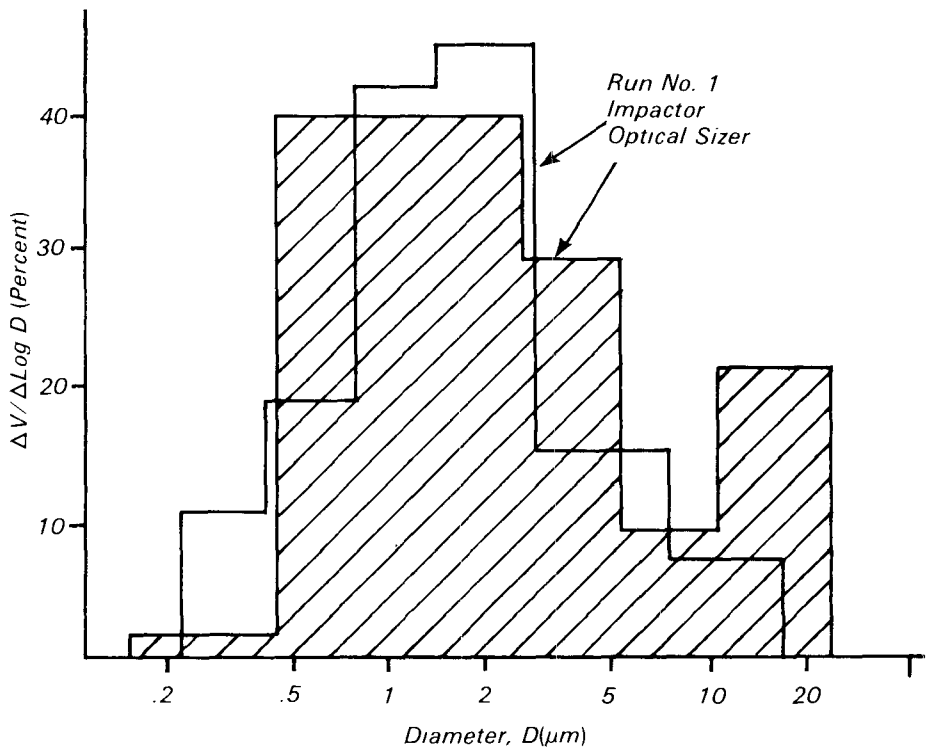


Figure 3. Particle size vs. volumetric concentration distribution during Day 1 of the field test

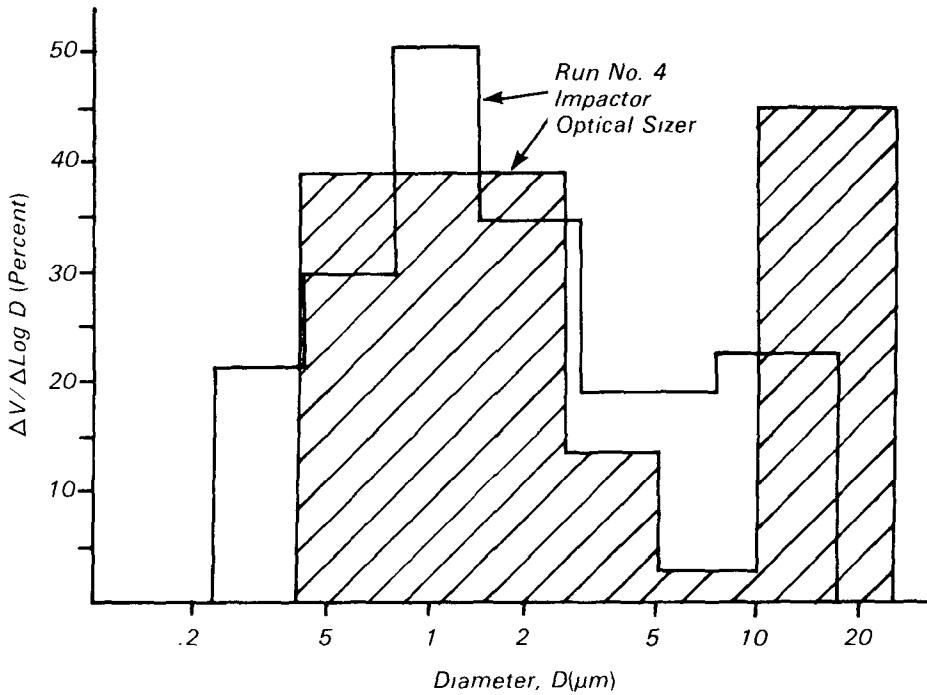


Figure 4. Particle size vs. volumetric concentration distribution during Day 2 of the field test

there are no moving parts in the prototype which would affect the calibration, some form of indicating calibration status is desirable.

Another area for future consideration is modification of the electronics to optimize the gain for loadings at or below the originally specified range of 0.01 to 0.1 grams/meter³. This could be done by changing the feedback resistors at the detector board and trimming the electrical offsets to lower values.

In its present form, however, this type of instrument should prove to be very useful for field survey work for analysis of size distributions from stationary sources. Recommendations for future work involve additional field trials at sites with different types of fuel, clean-up devices, and loading conditions. To gain confidence in this type of instrumentation, measurements with referee sizing instruments should be taken in parallel

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