

**A Study of the Relevant Incineration Technologies
and Air Pollution Control Devices
for the
Delaware Sand and Gravel Landfill**

**Submitted by: Andrew Clibanoff
NNEMS Project Control Number: U-913442-01-0
September 14, 1990**

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Abstract

The Delaware Sand and Gravel Landfill, located in New Castle County, DE, is an NPL site in its remediation design phase. A Record of Decision has mandated use of on-site incineration to dispose of approximately 25,000 cu. yd. of contaminated soils and wastes. This paper discusses the incineration technologies that may be applicable to the project and recommends the selection of a rotary kiln incinerator, based on the kiln's relative versatility when compared to the other incineration technologies. A study of air pollution control equipment was also included in the paper. No special permits for PCB incineration are required for this project, as PCB concentrations are below 50 ppm, the TSCA regulated standard. Emission of dioxin and related organic compounds can be prevented or minimized by maintaining a temperature above 1700°F in the afterburner. There is a definite need for more sampling of the wastes and soils that are going to be incinerated. The majority of sampling to date has been on soils surrounding the suspected highly contaminated areas. Further waste characterization must be completed before the final design of the incinerator and air pollution control equipment can be accomplished.

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1.0 Introduction

This paper is submitted in fulfillment of the requirements of the National Network for Environmental Management Studies (NNEMS) program. The scope of this NNEMS project includes the assessment of the feasibility of incineration technology as a viable alternative in the remediation effort occurring at the Delaware Sand and Gravel Landfill, New Castle County, Delaware. The status of this site is that it is currently on the National Priorities List (NPL) and is awaiting final remediation design. A remedial investigation report and feasibility study were completed in early 1988. A record of decision (ROD) has been written calling for the on-site incineration of the contaminated materials (waste and soil) that have been linked to groundwater degradation.

The paper will first present a site history and background, followed by a section on the relevant incineration and emission control technologies.

2.0 Background and Site History

The Delaware Sand and Gravel Landfill was an industrial waste landfill officially operating from 1968 through 1976. The landfill is approximately 27 acres in size and is located about two miles southwest of New Castle County, Delaware. Directly west of the site across Army Creek lies the Army Creek Landfill, another Superfund site. It is believed that the environmental degradation occurring in the vicinity can be differentiated between the two adjacent landfills. Figure 1 is a site location map for the Delaware Sand and Gravel Landfill. The site, as suggested by its name, was once operated as a sand and gravel quarry.

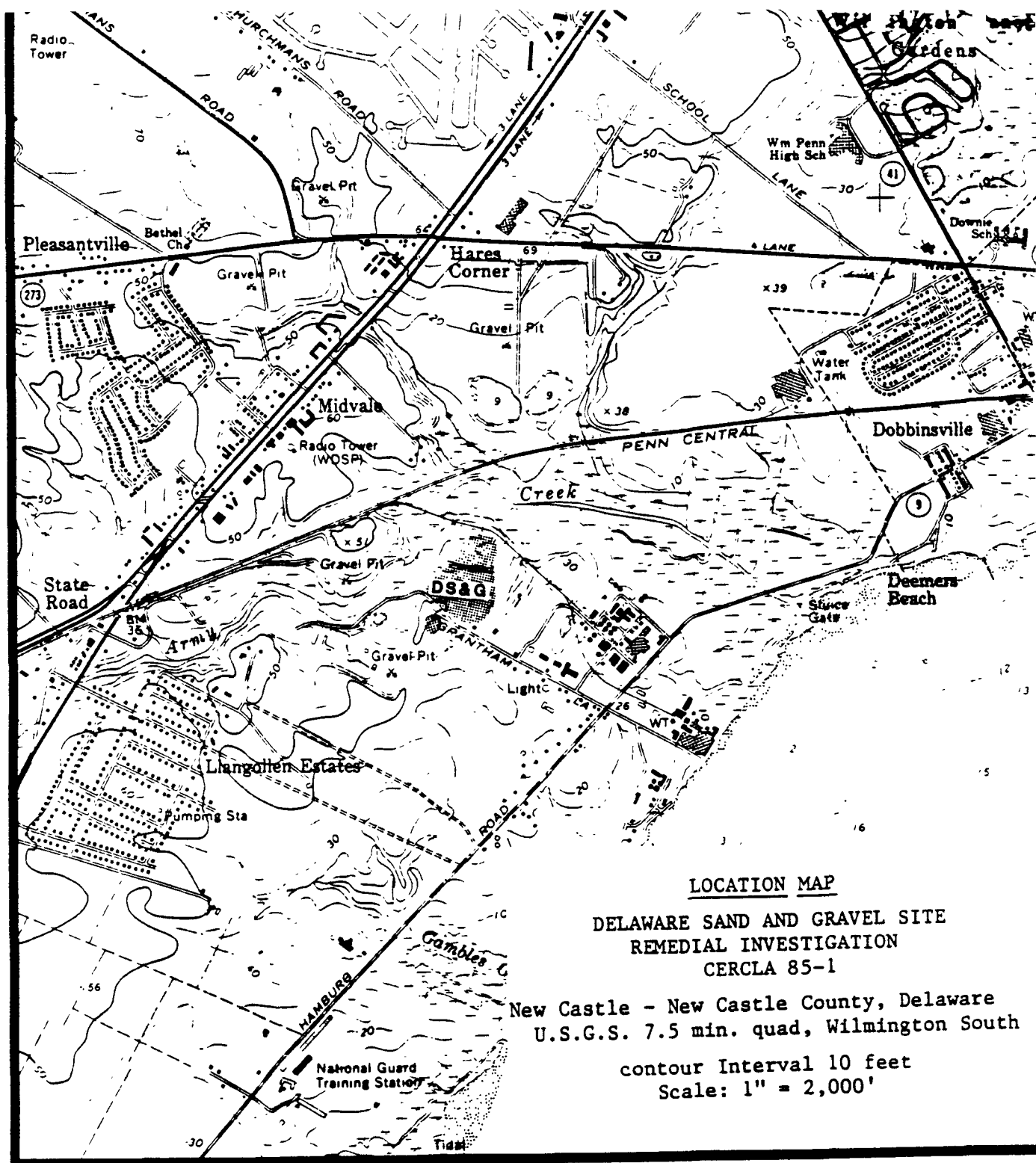


Figure 1

Location map for the Delaware Sand and Gravel Landfill
 (DS&G)
 SOURCE - FEASIBILITY STUDY (DUNN GEOSCIENCE CORP.)

In 1968, the Delaware Water and Air Resources Commission granted Delaware Sand and Gravel a Certificate of Approval for a sanitary landfill. One year later, an Air Pollution Control Permit allowed the disposal of cardboard, wire, pallets, corkdust, and styrofoam. In 1970, the Delaware State Board of Health issued a solid waste disposal permit to the facility. A Solid Waste Disposal Permit was issued from 1971 through 1976 by the Delaware Department of Natural Resources and Environmental Control (DNREC). In 1975, DNREC applied an enforcement action against the DS&G Landfill upon observation of improper operating procedures including poor cover and compaction.

2.1. Disposal Areas

Disposal of wastes at Delaware Sand and Gravel Landfill took place at four smaller areas on the site. These areas are termed the Drum Disposal Area, Ridge Area, Inert Area, and Grantham South Area. These areas, as well as the locations of boreholes, monitoring wells, and drinking water wells are depicted in figure 2. A further discussion of the individual waste disposal areas is below.

2.1.1. Drum Disposal Area

This area, located in the northern portion of the property, as shown in figure 2, accepted reportedly 7,000 drums containing industrial liquids and sludges from perfume, paint, plastics and petroleum refining processes. The Drum Disposal Area was reported to be a pit approximately 150 ft. x 70 ft. x 15 ft. or 0.23 acres in surface area. However, the areal extent of the Drum Disposal Area proper was delineated by surface geophysical data and measured to actually be 0.42 acres. This estimate does not include an

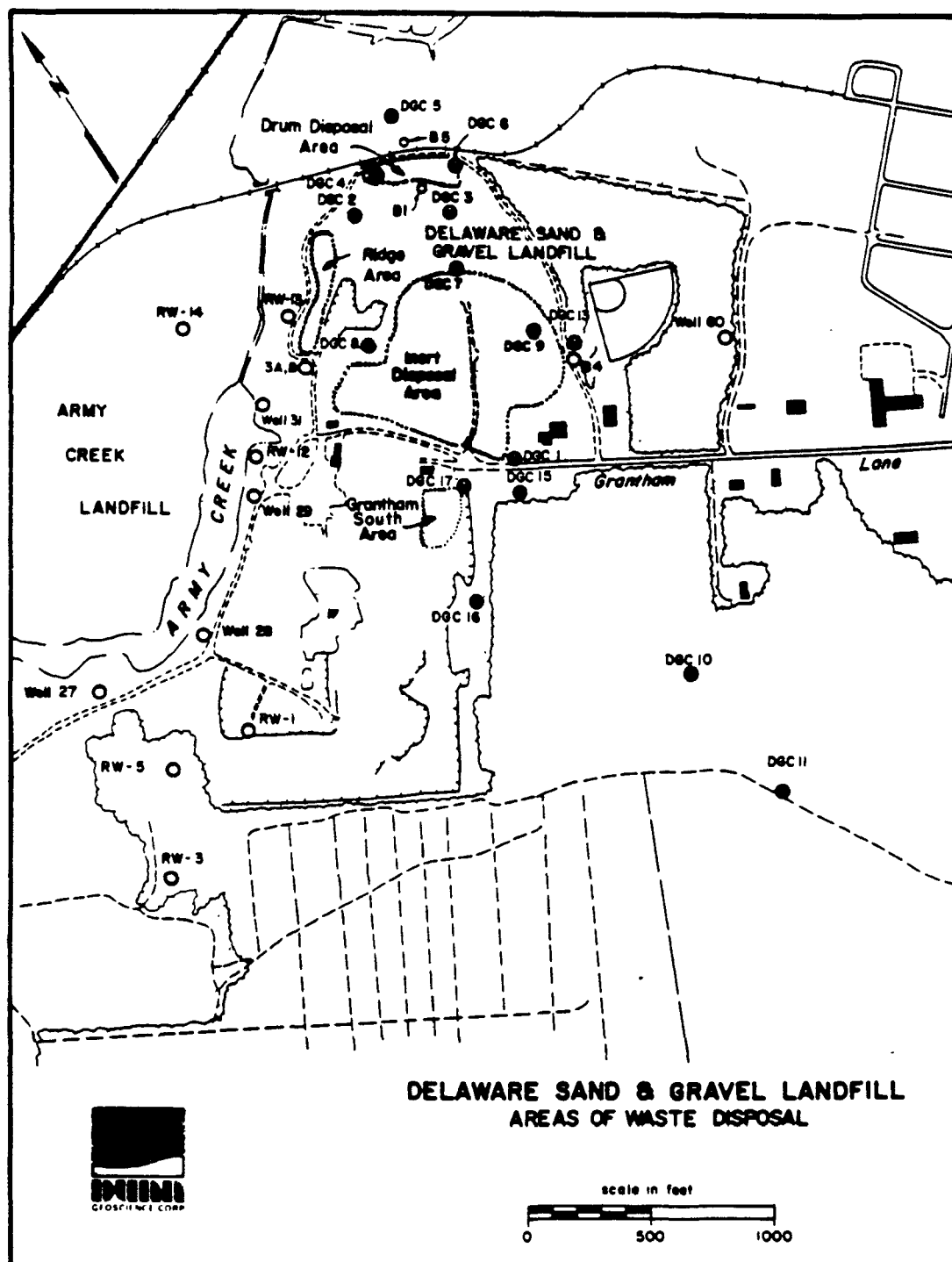


Figure 2: Areas of Waste disposal in the DS&G Landfill.

* SOURCE : FEASIBILITY STUDY (DUNN GEOSCIENCE CORP.)

adjacent 0.25 acre area just west of the Drum Disposal Area proper where an additional geophysical anomaly was detected.

Soil quality analyses of samples from boring DGC-06 (just east of Drum Disposal Area proper) indicates contamination of organics in the low parts per million range over an approximate depth interval of 5 to 30 ft. (see appendix B). If there truly is a 25 ft. depth of contaminated materials, the volume of materials requiring treatment may range from 20,000 cu. yd. to over 27,000 cu. yd. depending on whether the adjacent area is actually contaminated. However, boring DGC-04, west of the adjacent area shows little to no sign of contamination. Boring DGC-05, north of the area adjacent to the Drum Disposal Area proper also appears to be clean. It is quite clear that more sampling is needed to determine more accurately the extent of contamination in the soils of the Drum Disposal Area.

2.1.2. Ridge Area

This area, approximately 0.5 acres in size, is located on the western portion of the property, just east of recovery well RW-13 (figure 2). The Ridge Area contains scattered wastes (drums, large storage tanks, pallets, etc.) on the slope surfaces and ridge top. This area has been labeled as a limited drum and industrial waste disposal area.

2.1.3. Inert Area

This area, close to eleven acres in size, is located in the central southern portion of the DS&G property. Wastes disposed of in this area are assumed to be, as the name implies, relatively inert. The area is relatively level with steep side slopes and high vegetative growth. The surface is heavily littered with items such as junked cars, trucks, trailers, concrete forms, gas cylinders, domestic trash, paper rolls and wire bundles. Waste can

also be seen protruding from the sides of the slopes indicating that waste had been buried

2.1 4. Grantham South Area

This area, approximately 1.3 acres in size is located immediately south of Grantham Lane, directly across the street from the Inert Disposal Area (figure 2). It was reported that when the sand cliff remaining from quarrying behind the landfill owner's home began to erode, the owner backfilled the area presumably with inert waste. Reports from the owner's ex-wife as well as visual observations indicate that chemical wastes were disposed in this area as well.

2.2 Nature and Extent of Contamination

As mentioned earlier, the Delaware Sand and Gravel Landfill was operated as a permitted facility from 1968 to 1976. It is believed that dumping may have begun as early as 1961 and the dumping of household and construction wastes has continued to the present. The wastes disposed of at the site were mostly construction and industrial type wastes.

In 1984, a removal action was performed at the Drum Disposal Area. Several hundred drums were sampled and removed from the landfill's surface eliminating any immediate threat to human health and the environment. 576 drums were sampled with the results shown in table 1. It is believed that the remaining 7,000 - 100,000 drums in the Drum Disposal Area contain similar wastes. It is believed that the contamination at the Ridge Area is similar to that found at the Drum Disposal Area. The Grantham South and the Inert Disposal Areas are both believed to contain mainly inert wastes, such as wood, wire, hose, cardboard, styrofoam, etc.

<u>Type</u>	<u># of Drums</u>	<u>Estimated Volume</u>
Organic Solids	206	7,700 gallons
Inorganic Solids	201	6,900
Base/Neutral Liquids	37*	690
Flammable Solids	97	3,700
Base/Neutral Liquids pH 12	2	69
Acids	2	27
Organic Liquids	19	400
Contaminated PCB Solids	6	200
Contaminated PCB Liquids	2	27
PCB Solids	2	55
PCB Liquid	2	40

* includes 2 drums of flammable base/neutral liquids

Table 1 : 1984 Drum Removal Sampling Results
Source: RI Report

There has been evidence that the waste products disposed at the Delaware Sand and Gravel Landfill, particularly from the Drum Disposal and Ridge Areas, are leaching and causing environmental degradation of the surrounding area. The groundwater in the Upper Potomac Hydrologic Zone and on-site soils appear to be suffering the most. The predominant contaminants are iron, manganese, benzene, toluene, xylene, MEK, and MIBK with maximum concentrations of the organics in the low parts per million range. An overview of the air, water and soil environmental quality at the site is given below.

2.2.1 Air

The ambient air quality at the DS&G Landfill shows no evidence of air contamination with respect to volatile organics above background levels. A soil gas survey performed at the Grantham South Area did not detect any significant areas of volatile organic contamination. Only one sample had significant concentrations (2-9 ppm) of volatile organics. This probably indicates a small, isolated gasoline spill since the compounds detected strongly resembled oil or gasoline components. Therefore, the air currently poses no threat to the surrounding community. However, once remediation begins to take place, efforts must be undertaken to minimize the hazards of the potential air pollution problems associated with excavation and incineration.

2.2.2 Water

2.2.2.1 Surface Water and Stream Sediments

No significant degradation attributed to the Delaware Sand and Gravel Landfill could be found in the water and sediments from Army Creek, the Gravel Pit pond, or the intermittent stream east of DS&G. In fact, the quality

of water in Army Creek downstream of DS&G is actually better than it is upstream. However, even downstream, Army Creek is still polluted as there is evidence of stress on aquatic life.

2.2.2.2 Groundwater

As briefly mentioned earlier, groundwater quality within the Upper Potomac Hydrologic Zone (UPHZ) has been degraded with respect to inorganic and organic parameters in the DS&G vicinity. A distinct plume of organics and metals appears to be emanating from the Drum Disposal Area. The predominant contaminants identified in this plume are benzene, toluene, xylenes, ethyl benzene, bis (2-chloroethyl) ether, MIBK, MEK, iron and manganese. All analytical data on water can be found in appendix A.

Groundwater quality degradation was first noticed in late 1971 when a domestic well in the nearby Llangollen Estates became contaminated. Evidence indicated that the source of the contamination was coming from the Army Creek Landfill. In response, New Castle County installed a system of recovery wells in 1973 and 1974 to protect the Artesian Water Company's drinking water wells for Llangollen Estates by intercepting contaminated groundwater. As it turns out, these recovery wells are now intercepting the wastes emanating from the DS&G Landfill. Figures 3,4, and 5 show the reduction of size of the chloride ion contaminant plumes over time. Chloride was chosen because it is generally regarded as a conservative ion which does not readily degrade, adsorb onto aquifer materials, or precipitate under normal groundwater conditions. It can be said with reasonable confidence that the recovery well system is containing the contamination in the site vicinity.

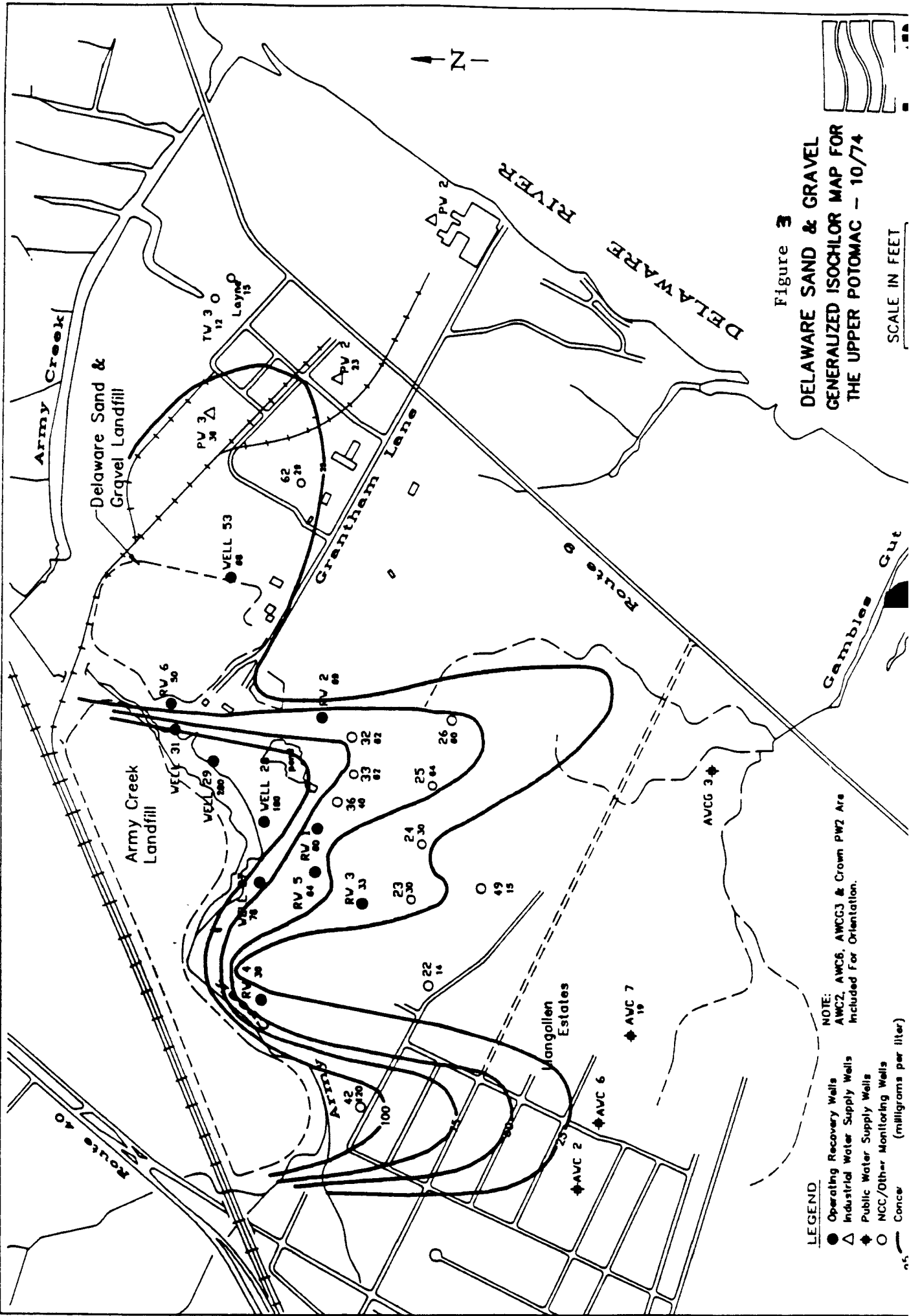
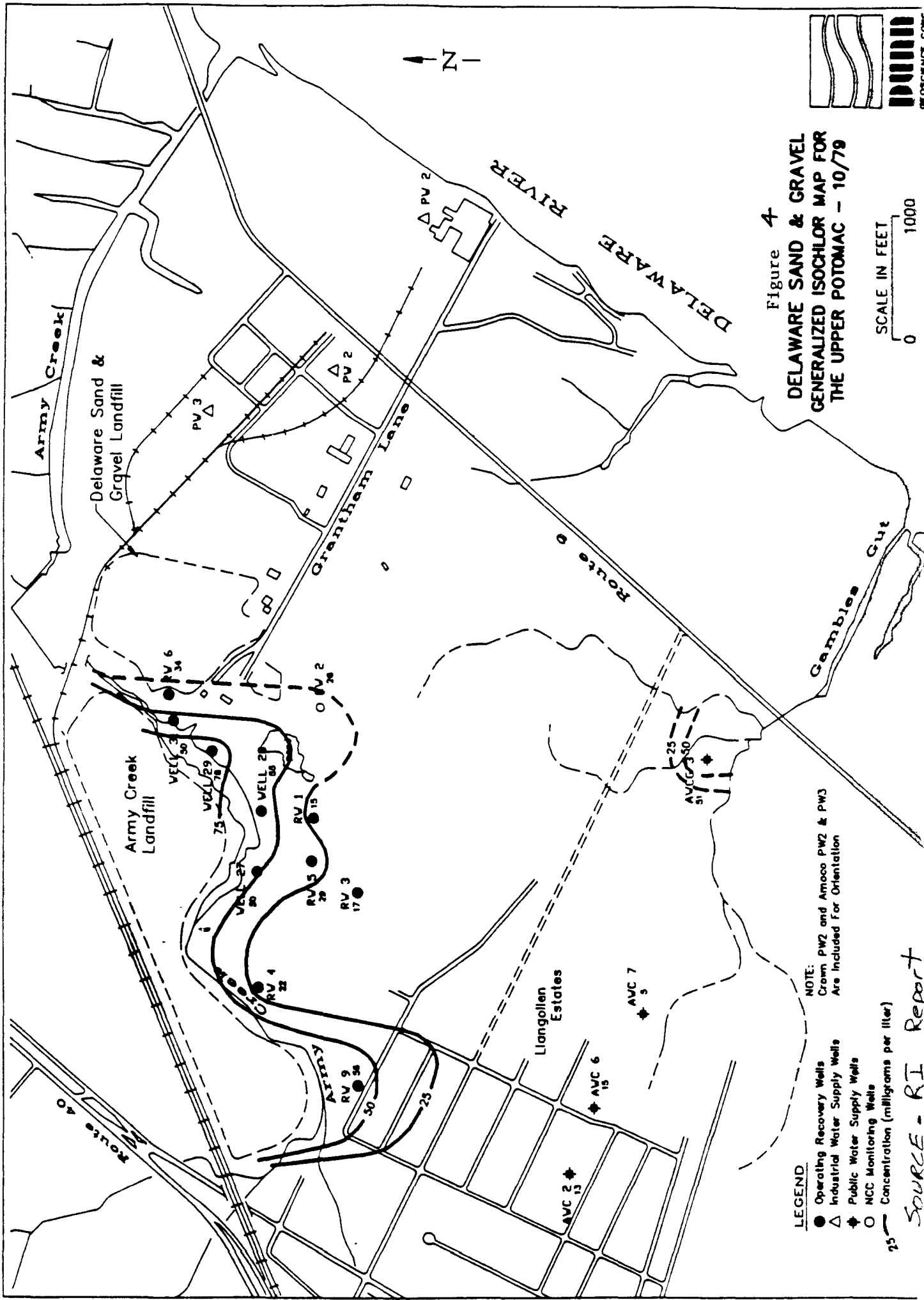
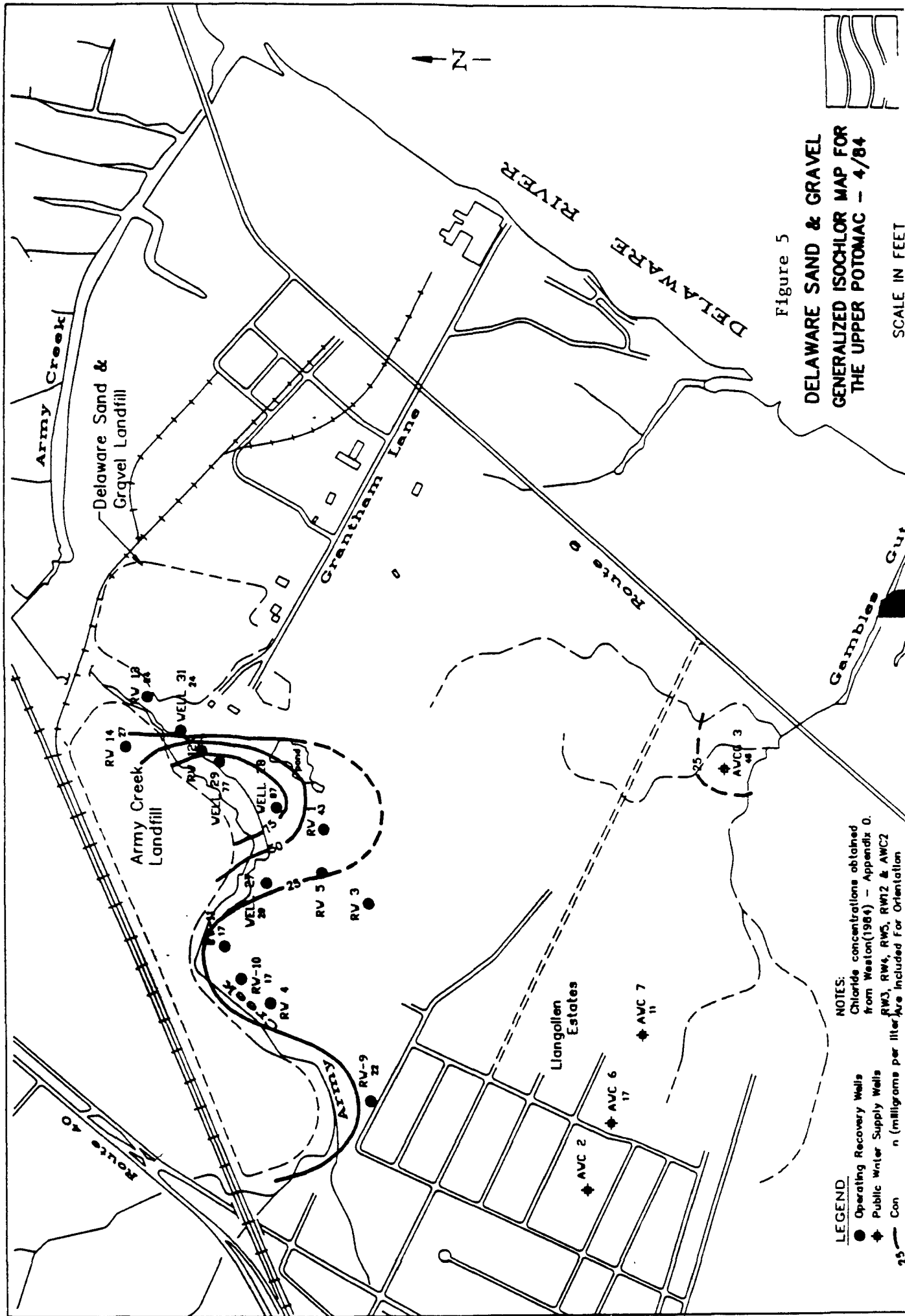


Figure 3
DELAWARE SAND & GRAVEL
GENERALIZED ISOCHLOR MAP FOR
THE UPPER POTOMAC - 10/74



SOURCE - RI Report



2.2.3 Soil

2.2.3.1 Surficial Soils

The analytical results (appendix B) for the surficial soils indicate isolated areas of contamination in both the Ridge and Grantham South Areas. One consideration that must be recognized is the fact that most of the surficial soils on site have been reworked by man. Much of the soils remaining on-site are the fines left over from the quarrying operation. These fines were used as cover material for the Inert and the Drum Disposal Areas. Therefore, any samples collected in these areas probably do not represent waste disposal.

2.2.3.2 Formation Soils

Analytical data (appendix B) from split spooned samples have indicated a plume of organics and metals emanating from the Drum Disposal Area and possibly some metal contamination emanating from the Inert Disposal Area. Organic compounds were detected in soil boring samples collected near the Drum Disposal Area, the base of the Columbia Formation close to the Drum Disposal Area, the uppermost Potomac silty clays beneath and adjacent to the Drum Disposal Area, and the top portion of the upper Upper Potomac sands.

2.3 Components of the Record of Decision

In early 1989, a Record of Decision (ROD) was drafted calling for the following measures to be taken in the remediation effort:

- Excavation of wastes and contaminated soils from the Drum Disposal and Ridge Areas. Treatment of these materials by on-site incineration to alleviate the direct contact threat and leachate generation from the major contamination sources on the site.
- Capping of the Grantham South Area to remove the direct contact threat and lessen leachate generation.

- Debris removal and capping of the Inert Disposal Area to remove the potential direct contact threat and to meet the Delaware State Solid Waste Regulations.
- Continued operation of the in-place recovery well system to eliminate potential groundwater ingestion risk.
- Implementation of recovered contaminated groundwater treatment system prior to discharge to Army Creek

3.0 Incineration Technology

Several recent laws or amendments make incineration one of the more favorable applications for hazardous waste remediation. The Superfund Amendments and Reauthorization Act (SARA) of 1986 placed new emphasis on the treatment of Superfund site wastes. \$8.5 billion has been authorized by SARA for Superfund cleanup from October, 1986 through October, 1991 (Cudahy, 1989). The RCRA Hazardous and Solid Waste Amendments of 1984 (HSWA) placed a land ban on untreated hazardous wastes beyond certain dates. The statute requires EPA to set levels or methods of treatment, if any, which "substantially diminish the toxicity of the waste or substantially reduce the likelihood of migration of hazardous constituents from the waste so that short-term and long-term threats to human health and the environment are minimized." (Esposito, 1988). Figure 6 is a summary of the suitability of the various technologies available for in situ waste destruction. Incineration technologies effectively address both of these RCRA concerns.

Incineration technology offers several attractive features for the treatment of hazardous wastes. It is immediate, requires a relatively small area for set-up and operation, and is a proven means of destruction for many organic wastes. When initially compared to other treatment methods, incineration appears to be costly. However, incineration will permanently destroy hazardous organics, removing the possibility of future liability for

Figure 6 In Situ Waste Treatment Technology Matrix.
(Adapted From Reference 1)

	Incineration	Pyrolysis	Wet Oxidation	Neutralization	Precipitation	Distillation	Air Stripping/ Soil Aeration	Activated Carbon	Evaporation/ Dewatering/ Phase Separation	Flotation	Extraction/Soil Washing	Membrane Sep / Ion Exchange	Evaporation	Filtration	Activated Sludge	In Situ Biodegradation	
Aqueous Wastes:																	
Metals	○	×	×	●	●	×	×	○	×	×	×	○	●	●	●	×	×
Highly Toxic	○	○	●	○	○	●	×	●	×	●	×	○	●	●	●	○	○
Organics	○	○	●	○	○	●	●	●	×	●	×	○	○	×	×	○	○
Volatile	○	○	●	○	○	●	●	●	×	●	×	○	○	×	×	○	○
Organics	○	○	●	○	○	●	●	●	×	●	×	○	●	●	×	●	●
Toxic Organics	○	×	×	×	○	×	×	×	×	×	×	×	×	○	●	×	×
Radioactive	○	×	×	●	●	○	×	×	×	×	×	×	×	×	×	×	×
Corrosive	○	×	×	●	●	○	×	×	×	×	×	×	×	×	×	×	×
Cyanide	○	○	●	○	○	×	×	×	×	×	×	×	×	×	×	○	×
Pesticide	○	○	●	●	●	●	×	●	×	●	×	●	●	●	●	○	×
Asbestos	×	×	×	○	○	×	×	×	×	×	×	×	○	●	●	×	×
Explosive	○	×	×	×	●	×	×	●	○	●	×	○	●	○	×	○	○
Organic Liquids:																	
Metals	○	○	×	●	●	●	×	×	×	●	○	×	×	●	●	×	×
Highly Toxic	●	●	●	×	×	●	×	○	×	○	×	×	×	×	×	×	×
Organics	●	●	●	×	×	●	×	×	×	○	×	×	×	×	×	×	×
Volatile	●	●	●	×	×	●	×	×	×	○	×	×	×	×	×	×	×
Organics	●	●	●	×	×	●	×	×	×	○	×	×	×	×	×	×	×
Toxic Organics	●	●	●	×	×	●	×	×	×	○	×	×	×	×	×	×	×
Radioactive	○	×	×	×	○	●	×	×	×	○	○	×	×	○	○	×	×
Corrosive	○	×	×	●	○	●	×	×	×	○	×	×	×	×	×	×	×
Cyanide	●	●	●	×	×	●	×	×	×	○	×	×	×	×	×	×	×
Pesticide	●	●	●	×	×	●	×	×	×	○	×	×	×	×	×	×	×
Sludges/Soils:																	
Metals	○	○	×	○	●	×	×	○	●	×	●	●	×	○	×	×	×
Highly Toxic	●	●	●	×	×	●	×	●	●	●	●	○	×	●	●	×	○
Organics	●	●	●	×	×	●	●	○	●	○	○	○	×	×	×	×	○
Volatile	●	●	●	×	×	●	●	○	●	○	○	○	×	×	×	×	○
Organics	●	●	●	×	○	○	×	●	●	●	●	○	×	○	○	×	●
Toxic Organics	○	×	×	×	×	×	×	×	×	●	●	×	×	×	×	×	×
Radioactive	○	×	×	●	×	×	×	×	×	●	●	×	×	×	×	×	×
Corrosive	○	×	×	●	×	×	×	×	×	○	×	×	×	×	×	×	×
Cyanide	○	○	●	×	○	○	×	×	●	×	○	×	×	×	×	×	○
Pesticide	●	●	○	×	●	○	×	●	●	○	●	●	×	●	○	×	○
Asbestos	×	×	×	×	×	×	×	×	●	×	●	×	×	×	×	×	×
Explosive	○	○	×	○	×	×	×	●	●	●	●	○	×	×	×	×	○
● Applicable ○ Potentially Applicable × Not Applicable																	

● Applicable

○ Potentially Applicable

× Not Applicable

Source: Brunner, 1988

their disposal. Most of the other treatment methods do not completely destroy the wastes, making future liability a distinct possibility (Brunner, 1988)

On-site incineration of hazardous wastes can be more appealing than transporting material to a central processing facility. On-site incineration avoids the high transportation costs as well as the NIMBY (not in my back yard) philosophy that can surround a central facility. On-site treatment is provided by situating modular-constructed facilities within the confines of the site.

3.1. General Incinerator Operation

Incineration is an engineered process using thermal oxidation of a waste material to produce a less bulky, toxic, or noxious material. A waste must be combustible to some extent in order for incineration to be considered as a possible treatment method. In running an efficient incineration process, the 3 T's of combustion, temperature, residence time and turbulence, must be controlled as closely as possible. The waste characteristics are likewise important parameters, including chemical structure and physical form. In the combustion process, the following reactions ideally take place.

- All hydrogen present converts to water vapor, unless otherwise noted below.
- All chloride (or fluoride) converts to hydrogen chloride, HCl (or hydrogen fluoride, HF).
- All carbon converts to carbon dioxide, CO₂.
- All sulfur converts to sulfur dioxide, SO₂.
- Alkali metals convert to hydroxides: sodium to sodium hydroxide ($2\text{Na} + \text{O}_2 + \text{H}_2 \rightarrow 2\text{NaOH}$) and potassium to potassium hydroxide ($2\text{K} + \text{O}_2 + \text{H}_2 \rightarrow 2\text{KOH}$).

- Non-alkali metals convert to oxides copper to copper oxide ($2\text{Cu} + \text{O}_2 \rightarrow 2\text{CuO}$), iron to iron oxide ($4\text{Fe} + 3\text{O}_2 \rightarrow 2\text{Fe}_2\text{O}_3$).
- All nitrogen from the waste, the fuel, or air, will take the form of a diatomic molecule, i.e., nitrogen is present as N_2

However, incinerators are not 100% efficient, and therefore may emit products of incomplete combustion (PIC). These PICs may be as hazardous or even more hazardous than the product in the waste feed. Therefore, some type of air pollution control device is usually required prior to discharge to the atmosphere.

3.2. Types of Hazardous Waste Incinerators

Currently in the marketplace, there are many different thermal technologies that have been recognized as potential treatment alternatives for hazardous wastes. The basic operation of each of these technologies is the application of heat (thermal) energy to the medium (soil) and contaminant. The increase in temperature causes the breakdown of the organic material. In most cases, this breakdown occurs under the presence of excess oxygen, and results in the combustion and destruction of the organic compounds.

The various incineration technologies may be classified as either high temperature or low temperature processes. High temperature processes are those which can heat soil to greater than 1000 °F while low temperature processes can heat soil to a maximum of 1000 °F. Examples of low temperature processes would be in-situ radio frequency, low temperature thermal aeration, and low temperature thermal stripping. There will be no further discussion of the low temperature processes in this paper as these processes are incapable of treating the more difficult compounds such as PCBs and dioxins. PCB contamination has been found at the DS&G Landfill.

The high temperature processes virtually guarantee the destruction of all organic constituents.

The types of high temperature hazardous waste incinerators currently available or soon to be available are : (1) Rotary Kiln, (2) Infrared, (3) Conventional Fluidized Bed, (4) Circulating Fluidized Bed, (5) Advanced Electric Reactor, (6) Plasma Arc, (7) Liquid Injection, (8) Molten Salt, and (9) Oxygen Burner. Of the nine listed technologies, the first four are the most applicable to the Delaware Sand and Gravel Landfill remediation effort and will be discussed in greater detail.

3.2.1. Rotary Kiln Incinerator

A rotary kiln is a cylindrical, refractory-lined shell mounted at an incline from the horizontal plane. Figure 7 depicts a typical rotary kiln incinerator. A rotary kiln system includes provisions for feeding, supplemental fuel injection, the kiln itself, an afterburner and an ash collection system. This type of incinerator is capable of handling solids, liquids, and sludges and would be applicable to the DS&G site.

When operating, the cylinder (primary combustion chamber) is rotated to promote mixing of the wastes with the combustion air and to aid in moving the waste through the reactor. Waste is deposited at one end and the waste burns out to an ash by the time it reaches the other end. The constant rotation also provides fresh surface exposure to oxidation which promotes destruction. A typical range for rotation would be from 0.75 to 4 rpm.

The gas stream, upon exiting the primary combustion chamber, is directed to an afterburner. The kiln will burn out solids and will volatilize organics. All the organics will generally not be incinerated in the kiln and a high temperature must be maintained at a specific residence time for

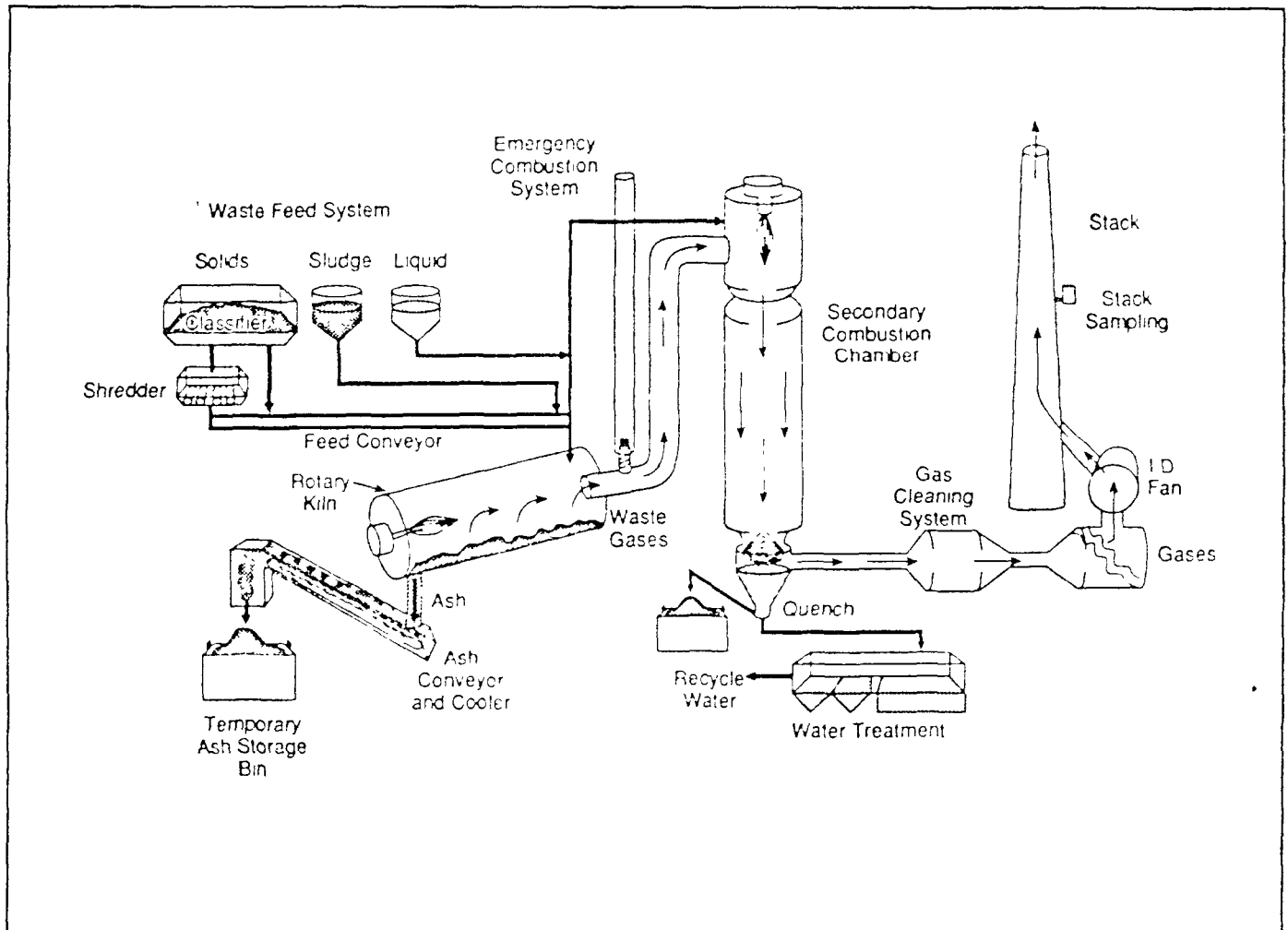


Figure 7: Rotary Kiln Incinerator.

Source: Johnson & Cosmos, 1989

destruction. This is the purpose of the secondary combustion chamber, or an afterburner.

The rotary kiln incinerator typically operates at temperatures between 1500 °F and 2900°F, with residence times of 0.5 - 2.0 hours for solids and two seconds for gases. Successful operation of rotary kilns have been demonstrated to have a destruction and removal efficiency of 99.9999% for wastes such as explosives, PCBs and dioxins. The rotary kiln is the most commercially available type of incinerator on the market today.

Advantages

- Not dependent on feed quality
- Fuel requirement follows feed loading, the less feed, the less fuel required
- Minimal waste pre-processing required
- Techniques exist for direct disposal of waste in metal drums
- Able to incinerate varied kinds of waste at the same time
- Many types of feed mechanisms available
- Residence time of waste in kiln readily controlled
- High turbulence and effective contact with air within kiln

Disadvantages

- Relatively high particulate carryover to gas stream
- Normally requires a separate afterburner for destruction of volatiles
- Unable to control conditions along kiln length
- Requires a relatively high amount of excess air (100-150 % of stoichiometric amount)
- Effective kiln seal is difficult to maintain
- Operation in a slagging mode to process inorganic wastes or metal drums increases kiln maintenance requirements

3.2.2. Infrared Furnace

The infrared furnace was developed and marketed by Shirco Infrared Systems of Dallas, Texas. The furnace consists essentially of a conveyor belt system passing through a long refractory lined chamber as shown in figure 8. Wastes are fed by gravity onto the belt and are immediately leveled to a depth

delivers pre-conditioned waste material to the primary furnace through a rotary airlock into the Spreading Section (2). There the material is spread and leveled on the Metering Conveyor (3) before entering the Feed Module (4). The Furnace Conveyor (5) moves the waste material through Fiber Blanket (6) insulated Powered Modules (7) where it is brought to combustion temperature by Infrared Heating Elements (8) and gently turned by Rotary Rakes (9). If residual material falls through the belt, it is collected in Hoppers (10) where it is removed by the center mounted Collector Screw (11) for analysis. Processed material (or ash) passes from the Discharge Module (12) into the Ash Discharge System (13) to an external receptacle.

The Combustion Air System (14) delivers air from a blower through manifolds to side ports. Exhaust gases are drafted through the furnace to the Exhaust Duct (15) and to the Secondary Process Chamber (16) to incinerate any remaining combustibles. Gases exit the secondary chamber and go through the base of the Emergency Bypass Stack (17) into the Emissions Control System (18) where they are cooled and cleaned before being exhausted by an Induced Draft Blower (19) through the Exhaust Stack (20).

The System Control Center (21) houses the primary controls to start, run, monitor and shut down all electrical and instrumentation subsystems.

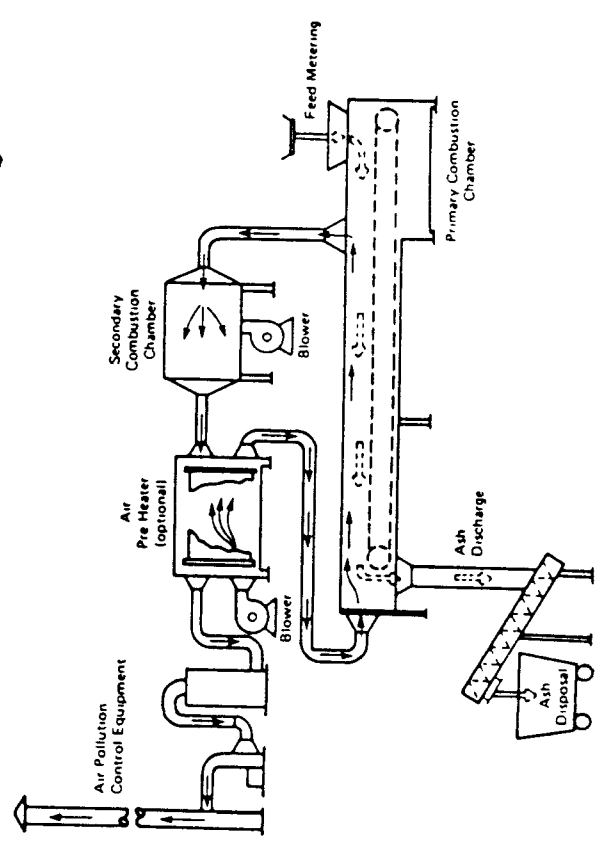
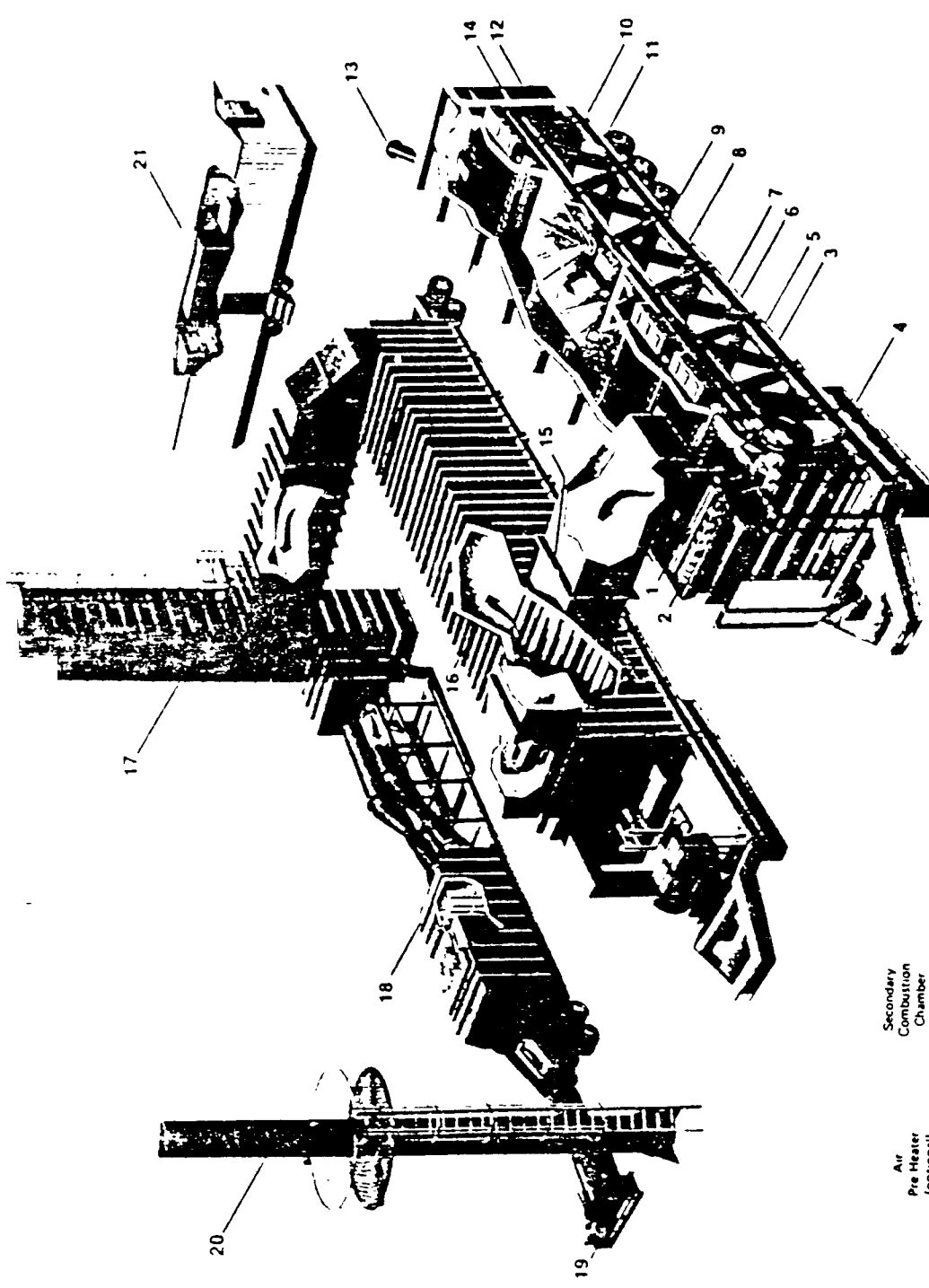


Figure 8: Infrared Incinerators
 Sources: Johnson & Cosmos, 1987
 Brunner, 1988

of two to three inches. The waste must be sized to no more than two inches in effective diameter. The belt speed and travel is chosen to provide burnout of the waste with minimal agitation. This feature results in a relatively low level of particulate emissions.

An induced draft fan maintains a negative pressure throughout the system. Combustion air is introduced at the discharge end of the belt so that waste and air travel countercurrently. Supplemental heat is provided by electric infrared heating elements within the furnace above the belt. The furnace is designed to provide and maintain a temperature of 1600 °F above the traveling conveyor. An afterburner is provided for destruction of volatiles.

The infrared furnace is capable of handling sludge cake, soil and other wastes. This alternative may be applicable to the DS&G site.

Advantages

- Not dependent on feed quality
- Low level of agitation of the product on the conveyor belt results in a smaller fraction of ash carryover to the gas stream
- The use of ceramic fiber insulation allows furnace to heat to operating temperature in less than two hours
- Furnace is applicable for intermittent or infrequent loading
- Heat generated by electric elements does not produce additional flue gas, as the burning of fossil fuels would
- The fuel requirement follows the feed loading rate
- Electric power elements are variable within their range
- Only 20-30% in excess of stoichiometric air requirements needed
- Minimal waste processing required
- Control of conditions along furnace length is readily available by separate control of individual heating elements and by varying air injection quality and location

Disadvantages

- Electric power costs four times that of fossil fuel
- When tied to existing power sources, installed kilowatt charges may be substantial
- An afterburner is normally required for the destruction of volatiles
- The mixing of fuel oil with soil to decrease electrical costs will generate additional flue gases

3.2.3 Conventional Fluidized Bed

The conventional fluid bed incinerator, figure 9, is a cylindrical refractory lined shell with a supporting structure above its bottom surface to hold a sand bed (fluidized bed). The structure has a series of tuyeres which allow the passage of air upward into the bed while preventing the passage of sand. Air, which is usually preheated, is introduced at the fluidizing air inlet at pressures from 3.5 to 5 psig. A high degree of turbulence is created in the sand bed by the passage of this air stream which creates motion on the top of the bed with the appearance of a liquid.

Waste is normally introduced within or just above the sand bed. The sizing of the furnace is a function of the moisture in the feed, the greater the moisture content, the larger the bed surface. Fluidization provides maximum contact of air with the waste surface to maximize the efficiency of the burning process.

Maintenance of the bed integrity is a function of the waste being combusted. The waste non-combustible content (ash) will either remain in the bed or become airborne and exit the furnace within the flue gas stream. Generally, sand has to be made up at the rate of approximately 5% of the bed volume every 100 hours of operation.

Because of intimate mixing of air and sludge in the fluid bed, excess air requirements are low, from 40% to 60%. The bed is maintained in the range of

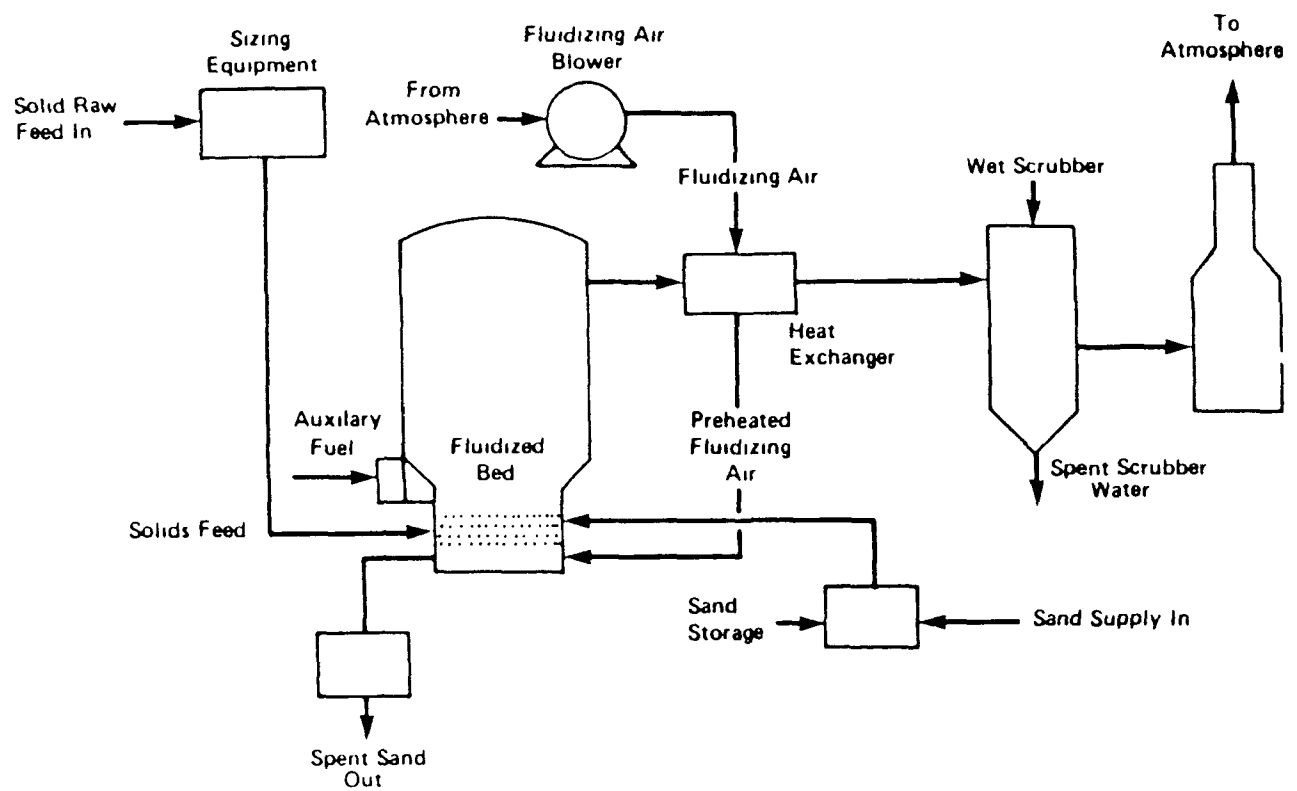


Figure 1 Conventional Fluid Bed Incinerator System.

Source: Brunner, 1988

1300 °F to 1500 °F, depending on the nature of the feed. The temperature of the freeboard (volume above the bed) is usually no more than 100 °F higher than the bed temperature. The residence time of gases in the freeboard is normally in the range of 3 to 6 seconds, usually enough time to alleviate the need for an afterburner. For example, if an organic compound that requires 2200 °F at a residence time of 1 sec. for four nines destruction is subject to a residence time of 5 sec., perhaps only 1600 °F may be required for the same level of destruction.

Advantages

- Design simplicity, few moving parts
- Excellent efficiency at rated load
- Thermally secure, able to be taken off line to hot standby without maintaining fuel feed
- High residence time in freeboard, afterburner usually not required
- applicable to the incineration of solids, liquids, and gases

Disadvantages

- Dependent on feed quality; test burns necessary to ascertain possibility of bed seizure when burning the material
- Poor efficiency at low loads
- Increase potential for air emissions compared to other systems
- Sand make-up is required on a continual basis
- Waste sizing is required
- Ash is discharged wet, dry ash discharge requires additional equipment

3.2.4. Circulating Fluidized Bed

The circulating fluid bed incineration system, developed by Ogden, Inc., is distinct from conventional fluid beds. In this incinerator, shown in figure 10, combustible waste is introduced into the bed along with recirculated bed material from the hot cyclone. A high air/gas velocity (from 15 to 20 ft/sec compared to 1.5 to 4.5 ft/sec in conventional systems) runs through the bed, causing the bed to rise through the reaction zone to the top of the combustion

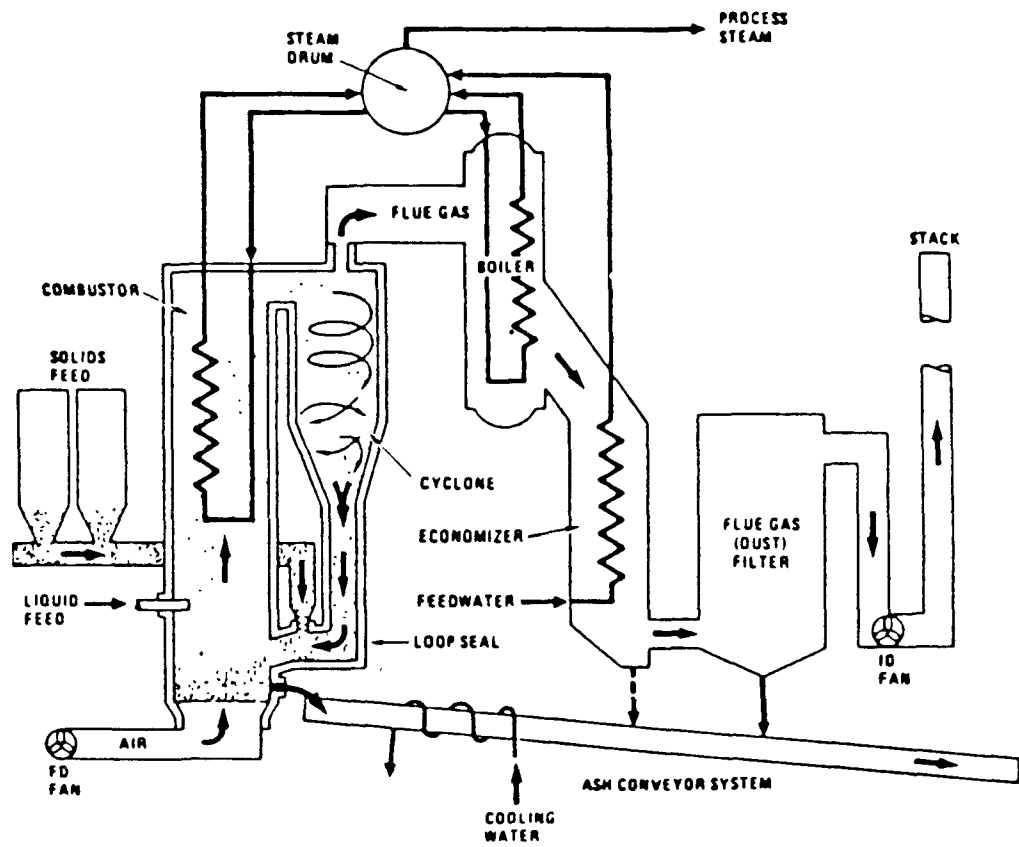


Figure 10 Circulating Fluid Bed Schematic.

Source: Brunner, 1988

chamber (freeboard) and pass through a hot cyclonic collector. Hot gas rise from the cyclone while the majority of solids drop to the bottom and are re-injected into the furnace bed. Flue gas exiting the cyclone passes through a conventional exhaust gas treatment system which removes particulate and other undesirable constituents from the gas stream.

Feed is introduced in the leg between the cyclone and the bed of the reactor. Solid or sludge waste is fed from a feeding bin using augers into the feed leg. Liquid or slurry wastes are pumped from a feed tank to the reactor. No atomizers or specialty nozzles are required for introduction of fluid wastes into the sand bed.

The design operating temperature is normally 1600 °F although the system can withstand temperatures up to 2000°F on a continuous basis. A major feature of the circulating fluid bed system is its ability to control the residence time of wastes to well over 15 seconds.

Advantages

- Same as conventional fluid bed plus:
- Can control residence time of wastes to over 15 seconds, thereby decreasing the temperature required for destruction
- Smaller particulate air emission potential than conventional fluid bed incinerator

Disadvantages

- Same as conventional fluid bed incinerator.

3.2.5 Advanced Electric Reactor

The Advanced Electric Reactor (AER) uses intense thermal radiation to heat wastes to between 4000 °F and 5000 °F. The AER consists of a vertical tubular core of porous carbon which is heated by electric heating elements. The waste is fed through the center of the core where the heated carbon transfers energy to the waste. This technology is not applicable because it is

not available in a full-scale model and the company that developed the pilot scale reactor, J. M. Huber Corp., has stated that their incineration services are no longer commercially available.

3.2.6 Plasma Arc

Plasma systems use the extremely high temperatures developed within the plasma stream to destroy hazardous organic wastes. The principle of plasma arc technology is the breaking of the chemical bonds between the elements of the organic constituents. This occurs in an atomization zone where a series of co-linear electrodes generate an electric arc, or plasma, which is stabilized by field coil magnets. As a low pressure air stream passes through the arc, the electrical energy is converted to thermal energy by the activation of the molecules of oxygen and nitrogen into their ionized atomic states. The temperature of the plasma arc will exceed 5,000 °F. When the excited atoms and molecules relax to lower energy states intense ultraviolet energy is emitted. This energy from the decaying plasma is transferred to the injected waste stream.

3.2.7 Liquid Injector

Liquid injection incinerators are one of the most commonly used incinerators for hazardous waste disposal. A liquid injection system contains a refractory-lined cylinder as a combustion chamber and usually another chamber for further combustion. Burners are normally located in the chamber in such a manner that the flames do not impinge on the refractory walls. The liquid waste, which must be converted to the gas phase prior to combustion, is initially atomized when it passes through the burner nozzles while entering the combustor. As the name implies, the liquid injection incinerator is confined to hazardous liquids, slurries and sludges with a

viscosity value of 10,000 SSU or less. Because the majority of wastes to be treated at the DS&G Landfill are in soils, the liquid injection incinerator is not applicable for this remediation effort.

3.2.8 Molten Salt Incinerator

The molten salt process is an oxidation and recombinant process where wastes are oxidized and/or chemically altered to innocuous substances. A salt bed (made up of either sodium chloride, sodium sulfate, sodium phosphate, sodium carbonate, or corresponding calcium salts) is heated to fluidization. Typical bed temperatures range from 1400 °F to 1600 °F. Waste components dissolve within the melt, producing an off-gas containing carbon dioxide, steam, oxygen, and nitrogen from the air supply. The off-gas will also contain particulate matter, salt and other components generated within the melt and elutriated into the stream. The molten salt acts as a dispersing medium for both the waste being processed and the air used in the reaction. The salt acts as a catalyst for oxidation reactions and accelerates the destruction of organic materials while preventing the discharge of acidic gases by neutralization. Ash generated, as well as other noncombustibles are physically retained within the melt.

3.2.9 Oxygen Burners

Oxygen burners or oxygen-enriched incineration are a technology that is essentially an improvement over existing burner designs wherein air enriched with oxygen is used in place of ambient combustion air. As oxygen replaces part of the combustion air, the nitrogen content of the gas stream through the incinerator is reduced accordingly. The advantage to this is that NO_x emissions can be reduced substantially. Other advantages also include.

- Incinerator throughput, normally limited by residence time requirements, blower capacity, and capacities of the off-gas

treatment units, can be increased significantly.

- Consumption of supplemental fuel (if required) is reduced because of a decrease in the sensible heat lost to the flue
- Improved DRE occurs as a result of longer residence times (in retrofitted installations) and a richer mixture.
- Off-gas treatment can be accomplished in smaller units and can be more effective.

The only disadvantage to oxygen burners is the added cost of the oxygen. I was unable to find any economic information regarding the cost of the operation of an oxygen-enriched incineration process.

3.3 Incinerator Selection

Table 2 shows the typical operating ranges of various incineration processes. Table 3 shows the applicability of various incineration processes to incineration of hazardous waste by type.

The best choice for the incineration of soils and wastes at the Delaware Sand and Gravel Landfill would be the rotary kiln incinerator. It is the most proven and commercially available incinerator on the market. The rotary kiln incinerator has become known as the workhorse of the industry. The rotary kiln can handle solids, sludges, and liquids all at the same time. Kilns used for incineration are batch fed with solids of varying shape, size, and heat content. This provides flexibility not available in other incinerator systems. Little to no pre-treatment of the wastes is necessary. The afterburner can reach temperatures up to 2900°F, more than high enough to completely destroy the most stubborn organic compounds. A number of transportable rotary kilns have been successfully operated throughout the United States.

The actual design of a rotary kiln system for the DS&G Landfill application takes quite a bit of time. The preparation of a detailed cost estimate of a complete incinerator facility takes about twelve engineer-weeks. Incinerator combustion chambers are sized on the basis of

TABLE 2. PERTINENT INCINERATION PROCESSES AND THEIR TYPICAL OPERATING RANGES

Process	Temperature range, °F (°C)	Residence time
Rotary kiln	1,500 to 2,900 (820 to 1,600)	Liquids and gases, seconds: solids, hours
Liquid injection	1,200 to 2,900 (650 to 1,600)	0.1 to 2 seconds
Fluidized bed	840 to 1,800 (450 to 980)	Liquids and gases, seconds: solids, longer
Multiple hearth	Drying zone 600 to 1,000 (320 to 540) Incineration 1,400 to 1,800 (760 to 980)	0.25 to 1.5 hours
Coincineration	300 to 2,900 (150 to 1,600)	Seconds to hours
Starved air combustion/pyrolysis	900 to 1,500 (480 to 820)	Tenth of a second to several hours

Source: Kinkhabwala, 1988

TABLE 3. APPLICABILITY OF AVAILABLE INCINERATION PROCESSES TO INCINERATION OF HAZARDOUS WASTE BY TYPE

Waste type	Rotary kiln ^a	Liquid injection	Fluidized bed ^a	Multiple hearth	Coincineration	Starved air combustion/pyrolysis
Solids						
Granular, homogeneous	X		X	X	X	X
Irregular, bulky (papers, etc.)	X				X	X ^b
Low melting point (tars, etc.)	X	X ^c	X		X	X
Organic compounds with fusible ash constituents	X			X	X	X
Unprepared large bulky material	X					
Gases						
Organic vapor laden	X ^d	X ^d	X ^d	X ^d	X ^d	X ^d
Liquids						
High organic strength aqueous wastes, often toxic	X ^e	X	X		X	
Organic liquids	X ^e	X	X		X	
Solids/liquids						
Waste contains halogenated aromatic compounds (2,400°F minimum)	X	X ^f			X	
Aqueous organic sludges	X ^g		X	X	X	

^a Suitable for pyrolysis operation

^b Handles large material on a limited basis

^c If material can be melted and pumped

^d If properly presented to the incinerator

^e If equipped with auxiliary liquid injection nozzles

^f If liquid

^g Provided waste does not become sticky upon drying

Source: Kinkhabwala, 1988

estimates of the flue gas volume generated by the burning of hazardous waste and auxiliary fuel. The costs of components downstream of the combustion chambers are a function of flue gas volumetric flowrate. Sampling and characterization of the actual wastes and soils to be incinerated is required (rather than the sampling of surrounding areas which is all that is currently available) before an effective design can be developed.

The cost for a rotary kiln incinerator may range from \$150 to \$350/ton (Liddicoatt, 1990). Assuming that there is 25,000 yd³ (20,500 yd³ from the Drum Disposal Area, 4,500 yd³ from the Ridge Area) of soil and wastes to be incinerated, the total incineration cost may be expected to range from \$8.4 million to \$19.5 million.

4.0 Incinerator Emissions

The use of hazardous waste incinerators has met a substantial amount of public opposition because people are concerned about the potential risks to human health and the ecosystem from stack emissions. This concern could be avoided if the general public had a better understanding of incineration emission potentials and available control techniques.

When hazardous wastes are burned with oxygen, they react to form combustion products, such as CO₂, CO, H₂O, HC and particulate matter. Significant amounts of other species are also normally released during incineration, including SO_x, NO_x, acids, salts, halogenated organics, free halogen gases, and amines. The stack gas may contain partially burned hydrocarbons such as benzene, carbon tetrachloride, chloroform, benzene hexachloride, benzo-a-pyrene, and dioxins in the stack gas. These compounds are of concern because they are toxic and carcinogenic at low exposure levels.

Many metals are of concern in hazardous waste incineration because of the possible adverse human health effects associated with exposure to emissions of these elements and/or their compounds from incinerator stacks. Metals of primary interest include arsenic, barium, beryllium, chromium, cadmium, lead, mercury, antimony, silver and thallium.

4.1 Types of Emissions

4.1.1 Particulate Matter

The term particulate matter, comprises a complex category of materials, both solid and liquid, that inhabit the atmosphere. The size range of particulates (also known as aerosols) ranges from 0.1 micron (μ) to 500 μ in diameter. Particles larger than 10 μ can be seen with the naked eye. Particulate matter may originate from inorganic or organometallic substances introduced with the waste, auxiliary fuel, combustion air, or some combination of these materials. Inorganic matter, such as salts and trace metals present in the waste and fuel, are known as ash and cannot be destroyed by incineration. The ash content is usually much higher in solids and sludges than in liquid wastes. Emissions of particulate matter are influenced by the chemical composition of the waste and the auxiliary fuel being incinerated, the type of incinerator and its operating parameters, and the air pollution control system. Most of the pollutants of concern, such as heavy metals and organic toxic byproducts, will condense either as fine particles or on fine particles as the exhaust gas stream cools.

As the quantity of metallic constituents in the feed increases, the quantity of metallic oxides also increases. These particulates are mostly less than one micron in size, and they may include oxides of silicon, sodium, calcium, zinc, magnesium, iron and aluminum with lower percentages of trace

metals. The oxide particles reflect light and produce highly visible emissions which appear worse than stack test results would indicate

The technology for particulate control is well developed. Selection of control equipment depends on several factors such as the inlet grain loading, particle size distribution, acid removal devices and regulatory requirements. Scrubbers, baghouses and wet electrostatic precipitators are currently used on hazardous waste incinerators. Many engineers use quenchers, which serve both to cool the gases and to permit particulate growth, followed by medium to high energy venturi scrubbers for ultimate capture. Alternate designs involve precipitators (either wet or dry) followed by absorbers for the gas components.

4.1.2 Gaseous Matter

Flue gas will normally have components classified as either organic or inorganic. Inorganic gases produced from the burning process normally include carbon dioxide, carbon monoxide, oxides of nitrogen, and oxides of sulfur (if present). Emission of carbon monoxide is normally very low due to the high-level combustion and destruction efficiencies achieved in the hazardous waste incinerators, but emissions of nitrogen oxides are usually high due to thermal fixation of oxygen and nitrogen in the combustion air at high temperatures. Depending on the waste, emission of oxides of sulfur and other various acid gases may also result from hazardous waste incineration. The acid gases emitted may include sulfur dioxide, hydrogen chloride, hydrogen fluoride, and hydrogen bromide. Various scrubbing technologies are available to control all of the above acid gases. Carbon dioxide is currently not considered an air pollutant.

Possible organic gas emissions may include oxygenated hydrocarbons, halogenated hydrocarbons, olefins, and aromatics. Emissions of any type of hydrocarbon are normally very low because of the destruction efficiency of the high-temperature combustion process. Incineration of chlorinated hydrocarbons results in the formation of hydrochloric acid and free chlorine. The chlorine results from an inadequate supply of hydrogen to convert the chlorine in the compounds to hydrochloric acid. Since many chlorinated organics often require an auxiliary fuel for their proper destruction, it is advisable to use natural gas as this will aid in the conversion of the chlorine to HCl.

4.1.3 PCBs

Incineration of substances containing PCBs (polychlorinated biphenyls) is covered by the Toxic Substances Control Act (TSCA). Permitting under TSCA is reserved for EPA. Under TSCA a material containing less than 50 ppm PCBs is not controlled. TSCA mandates that for destruction of PCBs, combustion at 1200 °C with a 2 second retention time and 3% oxygen in the exhaust gas or 1600 °C with a 1.5 second retention time and 2% oxygen in the exhaust is required. Additionally there must be a combustion efficiency of at least 99.9%.

However, at NPL sites, such as the DS&G Landfill, RCRA and TSCA incineration permits are not required. At these sites, the EPA Regional Administrator sets the applicable standards, which may include compliance with the provisions of incinerator permitting under TSCA without the necessity of obtaining an actual permit.

From the analytical data currently available for the DS&G Landfill, the PCB contamination is below the 50 ppm level. However, the need for further

sampling and waste characterization is evident before any final incineration design is implemented.

4.1.4 Dioxin

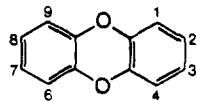
Trace quantities of dioxins have been reported to have been found in the emissions of hazardous waste incinerators. The term dioxin is a generalization of a family of chlorinated organic compounds consisting of two benzene rings connected by two oxygen bridges. When chlorine atoms occupy two or more of the eight available locations on the two benzene rings, the resulting molecule is known as a polychlorinated dibenzo-p-dioxin (PCDD), or dioxin for short. Of the 73 different possible varieties of dioxins, 2,3,7,8-TCDD is the most toxic found to date. PCDDs are thermally stable up through 1300°F and have an extremely low vapor pressure. Figure 11 shows dioxin and some related compound chemical structures.

Although no cases of human death or even long-term disability have been attributed to dioxins in the United States or elsewhere, 2,3,7,8-TCDD was found to be extremely toxic to small animals. It is the most toxic synthetic chemical known, 500 times more potent than strychnine and 10,000 times more potent than cyanide as determined by laboratory analysis. Some observations pertaining to dioxin's human health effects are:

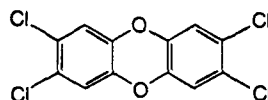
- In each case of exposure a skin disorder, chloracne, has occurred. Chloracne is a severe facial eruption and is a severe irritant.
- Liver damage has been reported a number of months after exposure. However, in each case, signs of this damage have disappeared within a period of two to five years.
- No human symptoms or reactions have been found to be permanently injurious to well-being
- Although no relationship to malignancies has been found between dioxins and human life, this is a fear, particularly as a long-term effect.

2,3,7,8-TCDD is one compound in a family

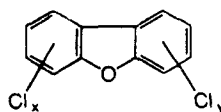
All dibenzo-*p*-dioxins have a three-ring structure consisting of two benzene rings connected by oxygen atoms:



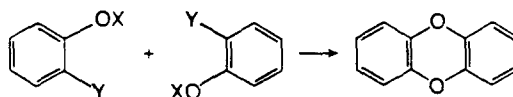
And 2,3,7,8-tetrachlorodibenzo-*p*-dioxin is one of the 75 possible chlorinated dioxins:



Related are chlorinated dibenzofurans:



Dioxin precursors combine to form dioxin in the general reaction:



For example, 2,3,7,8-TCDD is the most likely result from the reaction of 2,4,5-trichlorophenol:

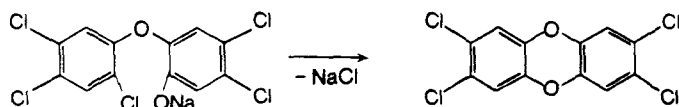
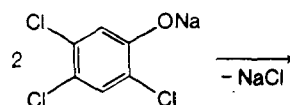


Figure 11: Dioxin and Related Compound Chemical Structure
Source: Worthy, 1983

There are many theories of how dioxin may form during incineration including the following:

- Burning of wastes which contain trace levels of PCDD will necessarily produce PCDD in the exhaust stream.
- The presence of two or more chlorinated organics act as precursors in the formation of PCDD. By a process termed *dimerization* these compounds will combine, under appropriate conditions of temperature and oxygen availability, to form PCDD.
- PCDD may be formed by partial oxidation of single-molecule precursor compounds, such as the partial oxidation of PCBs.
- The presence of chlorine and the chlorine (chloride) attack of basic aromatic hydrocarbon structures associated with lignin, such as wood, vegetable residues, etc., encourage PCDD formatio

Dioxins, as it turns out, are not very difficult to destroy. There is no unique thermal or kinetic stability attributable to dioxins that would prohibit its efficient destruction at high temperatures. The use of an auxiliary fuel and the availability of molecular oxygen reduce dioxin levels substantially. The probability of gas-phase formation of dioxin is very low at high temperatures, $\geq 1700^{\circ}\text{F}$, if mixing between fuel and air is efficient. More sampling and further waste characterization is required to estimate whether dioxin may be a problem at DS&G.

4.2 Air Pollution Control Devices

There are numerous types and sizes of air pollution control devices (APCDs) on the market today. They range from the unsophisticated, a series of baffles, to the relatively complex high-energy water scrubbing devices, utilizing alkali, to clean gas streams of solid, liquid, and gaseous pollutants. Below is a description of a few of the APCDs currently available.

4.2.1 Electrostatic Precipitator

In an electrostatic precipitator (ESP), a negative electrical charge is imparted on the particles in the flue gas. The negatively charged particles are then attracted and retained by positively charged collection electrodes. The particles are removed from the electrodes into collection hoppers by rapping. The process is carried out within an enclosed chamber made of metal or Fiberglass Reinforced Plastic. The grounded collecting electrodes (plates) are suspended within the chamber. Power input is provided by a high-voltage transformer and a rectifier. Discharge electrodes suspended between the plates are negatively charged with voltages ranging from 20 to 100 Kvolts. Figure 12 shows a typical electrostatic precipitator.

4.2.2 Wet Electrostatic Precipitator

Wet Electrostatic Precipitators (WESPs) are a relatively new technology and are generally used for applications where the potential for explosion is high or where particulates are very sticky. Figure 13 is a cross section through a wet ESP. They are basically the same technology as dry ESPs with the following two important distinctions:

- A wet spray is included in the inlet section for cooling, gas adsorption, and coarse particle collection
- The collection electrode is wetted to flush away the collected particles.

4.2.3 Fabric Filter (Baghouse)

Fabric filters remove dust and particles from the flue gas by passing the gas through a fabric bag. The cleaned gas exits from one side of the filter while the dust is collected on the other side. Baghouses are very efficient for gases containing small particles. The collected dust may be removed from the filter bag by any of three methods: mechanical shaking, reverse flow back-flushing at low pressure (reverse air), or reverse flow back-flushing at

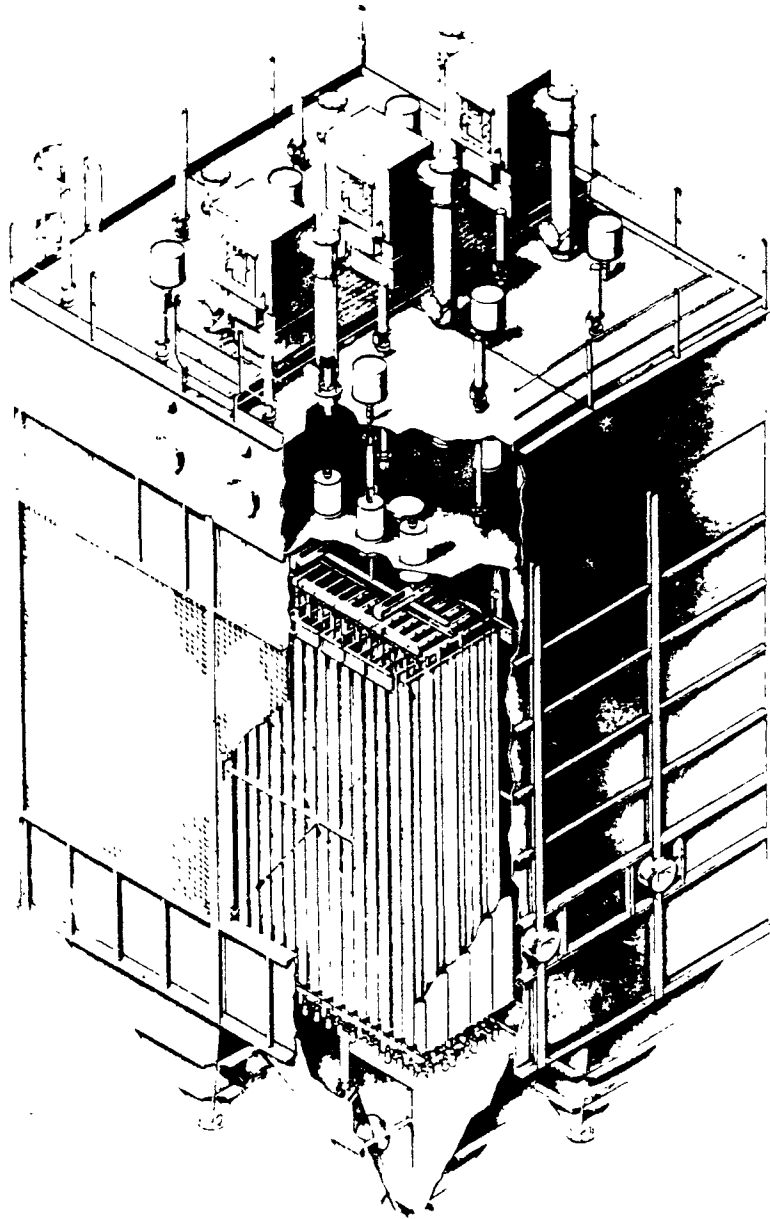


Figure 12 Typical electrostatic precipitator

Source: Brunner, 1986

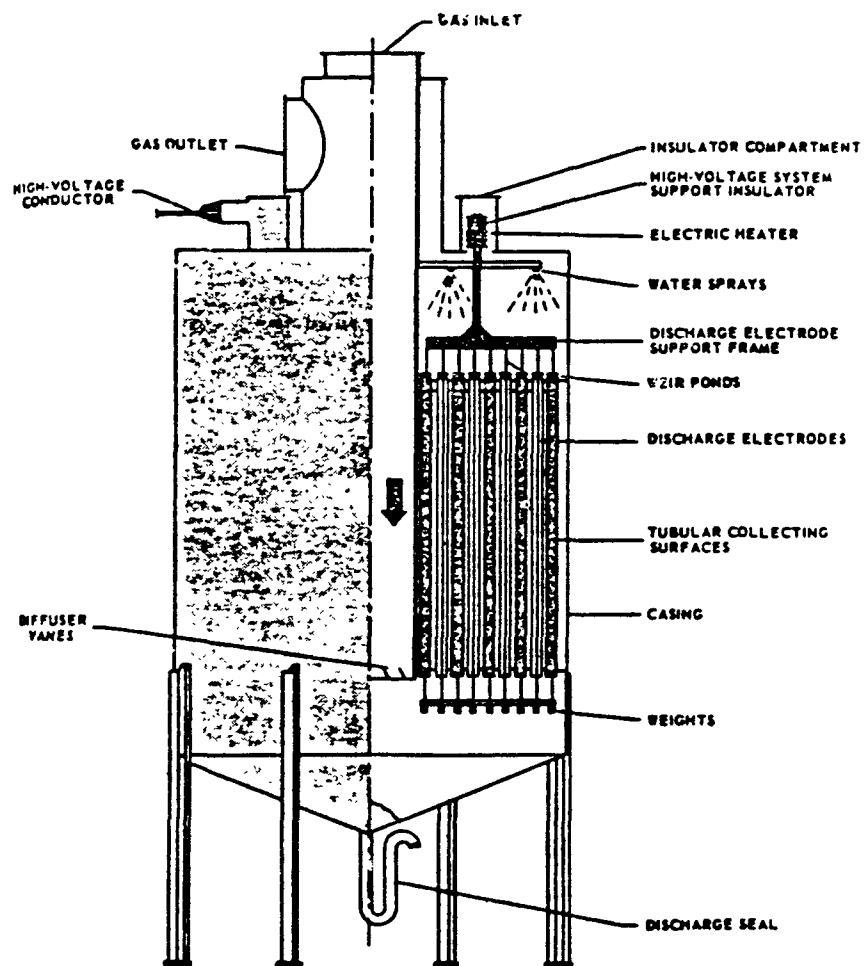


Figure 13 Tubular wet Electrostatic precipitator. (Source: Joy Manufacturing Co.)

Source: Brunner, 1986

slightly higher pressure (pulsed air). Figure 14 is a schematic of a bag filter with a shaker mechanism.

4.2.4 Quench Chamber

The quench chamber operates by passing the hot gases through a water spray. Quench chambers usually precede scrubber equipment in the pollution control treatment sequence, and are used to reduce the temperature of hot gases leaving the incinerator. The chamber also serves to protect the downstream equipment from high temperature damage and it reduces water evaporation in downstream scrubbing equipment. Figure 15 depicts an upflow quench reactor.

4.2.5 Wet/Dry Scrubber (Spray Dryer)

In the wet/dry scrubber, hot gases are passed through a fine mist of a dilute alkali slurry. The water in the slurry absorbs acids from the flue gas and the acids react with the alkali solids in the slurry to form salts. Water is lost through evaporation, leaving the salts and any unreacted alkali behind as a dry powder. This particle-laden flow then goes to a fabric filter or an ESP to remove the particulates. Wet/dry scrubbers are considered cleaner control systems than wet scrubbers, mainly because the waste material is dry particulates and no further liquid treatment is required, which significantly reduces the waste volume.

4.2.6 Venturi Scrubber

In the venturi scrubber, a liquid is introduced into a constricted area. High velocity gas, from 200 to 600 ft/sec at the throat, is also introduced to shear the liquid into fine droplets and to allow large surface area for mass transfer. From the expansion section of the venturi throat the gas enters a

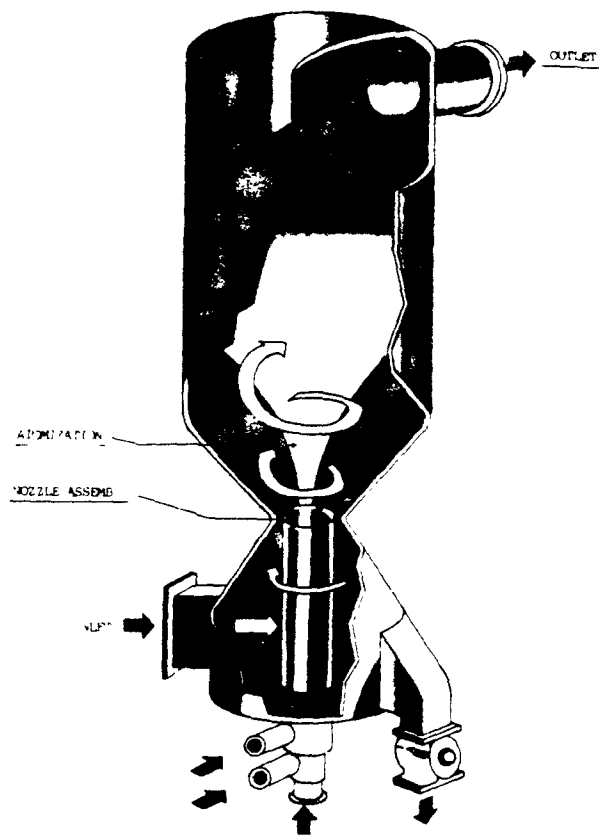


Figure 14 Upflow quench reactor.

Source: Brunner, 1986

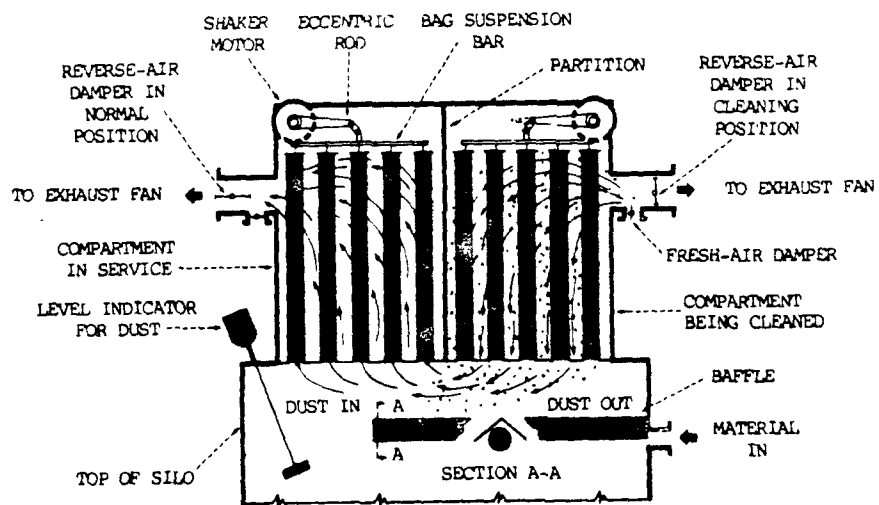


Figure 15 Bag filter with shaker mechanism.

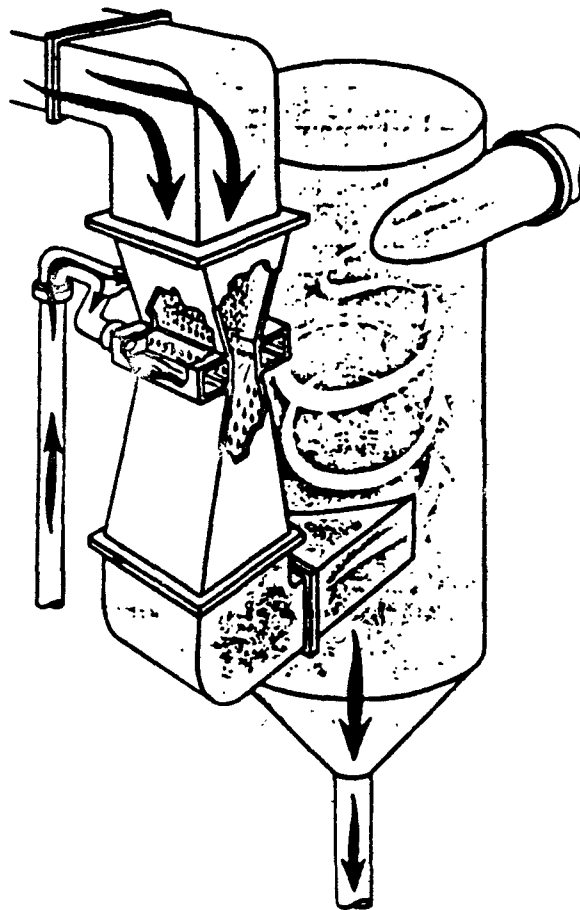


Figure 16 Venturi scrubber.

Source: Brunner, 1986

large chamber for separation of particles or for further scrubbing. Figure 16 illustrates a venturi scrubber where water is injected at its throat

4.3 Air Pollution Control Device Efficiency

Table 4 shows conservative estimated efficiencies of APCDs for controlling toxic metals emissions. Most toxic metals will condense as solids if incinerator combustion gases are cooled. As seen in the table, mercury is the least apt to condense prior to emission from the system stack as its degree of recovery above 400°F is generally slight. Quench chambers are frequently employed to cool flue gas prior to further treatment. Venturi scrubbers are frequently used while ESPs and WESPs are not widely used in hazardous waste incineration applications. Fabric filters have not been commonly used on hazardous waste incinerators as they are bulky and expensive, and require careful operation. At most facilities where data indicate high gas and particulate removal efficiencies, there are usually two to four APCDs in series. The particular series will depend on the type of incinerator and the characteristics of the wastes incinerated. A number of typical APC series are listed below:

- Quench/wet scrubber
- Quench/spray dryer/cyclone/ESP
- Quench/spray dryer/cyclone/fabric filter
- Quench/wet scrubber/ionizing wet scrubber/mist eliminator
- Quench/WESP/venturi scrubber/packed tower scrubbers
- Quench/venturi scrubber/packed tower scrubbers; and
- Fabric filter/wet scrubber

4.4 Selection of an Air Pollution Control Device Series

Further waste characterization studies and more sampling is required before the proper selection of an APCD series can be made. However, high levels of lead have been found in the sampling to date and it does not appear that mercury will be a problem. Therefore, the combination of a venturi

TABLE 4
Air Pollution Control Devices (APCDs) and Their Conservatively
Estimated Efficiencies for Controlling Toxic Metals

APCD	POLLUTANT				
	Ba, Be	Ag	Cr	As, Sb, Cd, Pb, Ti	Hg
*WS	50	50	50	40	30
*VS-20	90	90	90	20	20
*VS-60	98	98	98	40	40
ESP-1	95	95	95	80	0
ESP-2	97	97	97	85	0
ESP-4	99	99	99	90	0
*WESP	97	97	98	95	60
*FF	95	95	95	90	50
*PS	95	95	95	95	80
SD/FF; SD/C/FF	99	99	99	95	90
DS/FF	98	98	98	98	50
*FF/WS	95	95	95	90	50
ESP-1/WS; ESP-1/PS	98	98	98	90	80
ESP-4/WS; ESP-4/PS	99	99	99	95	85
*VS-20/WS	97	97	97	96	80
**WS/IWS	95	95	95	95	85
*WESP/VS-20/IWS	99	99	98	97	90
C/DS/ESP/FF; C/DS/C/ESP/FF	99	99	99	99	98
SD/C/ESP-1	99	99	98	95	85

* It is assumed that flue gases have been precooled in a quench. If gases are not cooled adequately, mercury recoveries will diminish, as will cadmium and arsenic to a lesser extent.

** An IWS is nearly always used with an upstream quench and packed horizontal scrubber.

C = Cyclone

WS = Wet Scrubber including:
 Sieve Tray Tower
 Packed Tower
 Bubble Cap Tower

PS = Proprietary Wet Scrubber Design

(A number of proprietary wet scrubbers have come on the market in recent years that are highly efficient on both particulates and corrosive gases. Two such units are offered by Calvert Environmental Equipment Co. and by Hydro-Sonic Systems, Inc.).

VS-20 = Venturi Scrubber, ca. 20-30 in W. G. Δp

VS-60 = Venturi Scrubber, ca. > 60 in W. G. Δp

ESP-1 = Electrostatic Precipitator; 1 stage

ESP-2 = Electrostatic Precipitator; 2 stages

ESP-4 = Electrostatic Precipitator; 4 stages

IWS = Ionizing Wet Scrubber

DS = Dry Scrubber

FF = Fabric Filter (Baghouse)

SD = Spray Dryer (Wet/Dry Scrubber)

Source: EPA Report 530/SW-90-041a, 1990

scrubber in series with a wet scrubber would appear to be adequate air pollution control for this application. Further examination of the regulatory requirements and the waste characteristics is needed before any official selection and design of air pollution control equipment is implemented.

5.0 Conclusion

The Delaware Sand and Gravel Landfill, an NPL site, is currently in the design phase of the remedial action. Wastes and soils from two areas, the Drum Disposal and Ridge Areas, are to be disposed by incineration. The total volume of material to be incinerated is expected to be between 25,000 yd³ and 30,000 yd³ depending on the actual boundaries and depths of wastes in the two disposal areas. The estimated range of costs for the incineration portion of the project is between \$8.4 million and \$19.5 million. These figures do not include excavation and handling and storage costs.

Much more sampling and waste characterization is required before the final design of the incinerator and any air pollution control equipment is begun. The best incinerator for the job right now appears to be the rotary kiln. This incinerator offers the most versatility of any of the incinerators currently on the market. It can handle solids, sludge and liquids at the same time with little or no pretreatment of the waste feed necessary. It is the only incinerator that can operate in a slagging mode in which it can reduce steel drums to a molten slag, a glass-like substance, when cooled. Transportable rotary kilns have been proven to be effective in similar applications throughout the country.

There are many types of air pollution control devices currently on the market that will bring the stack emissions within any applicable regulations. Venturi scrubbers, quench chambers and wet scrubbers are the most common pieces of equipment used today. For more complex applications, filter baghouses and electrostatic precipitators are available.

Incineration offers a permanent solution to the contamination problem occurring at the Delaware Sand and Gravel Landfill. It provides for the destruction of the hazardous or toxic components in the waste matrix and it reduces or eliminates the liabilities and risks pertaining to hazardous wastes.

References

- Bonner, T., Cornett, C., Desai, B., Fullenkamp, J., Hughes, T., Johnson, M., Kennedy, E., McCormick, R., Peters, J. and Zanders, D. Engineering Handbook for Hazardous Waste Incineration. National Technical Information Service, Springfield, VA. June, 1981
- Brunner, Calvin R. Hazardous Air Emissions From Incineration. Chapman and Hall, New York, 1986
- Brunner, Calvin R. Incineration Systems. Van Nostrand Reinhold Company, New York, 1984.
- Brunner, Calvin R. Site Cleanup by Incineration. The Hazardous Materials Control Research Institute, Silver Springs, Maryland, 1988.
- Cudahy, James, and Eicher, Anthony. "Thermal Remediation Industry: Markets, Technologies, Companies," Pollution Engineering, November, 1989.
- Devinny, J., Everett, L., Lu, J., and Stollar, R. Subsurface Migration of Hazardous Wastes. Van Nostrand Reinhold, New York, 1990.
- Dunn Geoscience Corporation, "Feasibility Study for the Delaware Sand & Gravel Landfill - Final Report" February, 1988.
- Dunn Geoscience Corporation, "Remedial Investigation Report on the Delaware Sand & Gravel Landfill." December, 1987
- EPA Report # 530/SW-90-041a. Guidance on Metals and Hydrogen Chloride Controls for Hazardous Waste Incinerators: Volume IV of the Hazardous Waste Incineration Guidance Series, 1990.
- Esposito, M., Taylor, M., Bruffey, C., and Thurnau, R. "Incineration of a Surrogate Superfund Soil Using a Pilot-Scale Rotary Kiln Incinerator," Unpublished draft report, 1988.
- Ives, Jim and Young, Derrell. "Hazardous Waste Incineration System Used on Alaskan Site," Oil and Gas Journal, Oct. 30, 1989.

Johnson, L., Midgett, R., James, R., Thomason, M., and Manier, M. "Screening Approach for Principal Organic Hazardous Constituents and Products of Incomplete Combustion," JAPCA, vol. 39, 1989

Johnson, Nancy, and Cosmos, Michael. "Thermal Treatment Technologies for Haz Waste Remediation," Pollution Engineering, October, 1989.

Kinkhabwala, Minesh, and Mehta, Ronald. "Case Study: Transportable Incineration Technologies for Permanent Superfund Remediations," Hazardous Waste Management Magazine, Jan.-Feb., 1988.

Liddicoatt, Carol. Review of Alternative Incineration Technologies for the Southern Maryland Wood Preservers Superfund Site, Hollywood, Maryland, Unpublished Report by Dames & Moore, 1990.

Rawis, Rebecca. "Dioxin's Human Toxicity is Most Difficult Problem," C&EN, June 6, 1983

Santolero, J. "Rotary Kiln Incineration Systems: Operating Techniques for Improved Performance," Hazardous and Industrial Wastes - Proceedings of the Twenty-Second Mid-Atlantic Industrial Waste Conference, Drexel University, Philadelphia, PA, July 24-27, 1990.

Shacklette, H. and Boerngen, J. Element Concentrations in Soils and Other Surficial Materials of the Conterminous United States. U.S. Geological Survey Professional Paper 1270. United States Government Printing Office, Washington, 1984.

Shaub, Walter and Tsang, Wing. "Dioxin Formation in Incinerators," Environmental Science & Technology, vol. 17, no. 12, 1983.

Shen, Thomas. "Hazardous Waste Incineration: Emissions and Their Control," Pollution Engineering, July, 1986.

Star, Alvin. "Cost Estimating for Hazardous Waste Incineration," Pollution Engineering, April, 1985

Timmons, D., Fitzpatrick, V., and Liikala, S. "Vitrification Tested on Hazardous Wastes," Pollution Engineering, June, 1990

Travis, C., Holton, G., Etnier, E., Cook, S., O'Donnell, F., Hetrick, D., and Dixon, E. "Potential Health Risk of Hazardous Waste Incineration," Journal of Hazardous Materials, vol 14, 1987.

Trenholm, Andrew, Lapp, Thomas, Scheil, George, Cootes, John, Klammer, Scott, and Cassidy, Carolyn "Total Mass Emissions from a Hazardous Waste Incinerator," Journal of Hazardous Materials, vol. 18, 1988.

Vogel, Gregory, and Martin, Edward "Cost File - Waste Incineration Part 1: Equipment Sizes and Integrated-Facility Costs," Chemical Engineering, September 5, 1983.

Vogel, Gregory, and Martin, Edward. "Cost File - Waste Incineration Part 2: Estimating Costs of Equipment and Accessories," Chemical Engineering, October 17, 1983.

Vogel, Gregory, and Martin, Edward. "Cost File - Waste Incineration Part 3: Estimating Capital Costs of Facility Components," Chemical Engineering, November 28, 1983.

Worthy, Ward "Both Incidence, Control of Dioxin Are Highly Complex," C&EN, June 6, 1983.

Appendix A

Analytical Data of Water and Groundwater at Delaware Sand and Gravel Landfill

Table 5.17
Inorganic Analytical Results for Surface Water

Inorganic Analytical Results of April 1985
Delaware Sand and Gravel RI/FS Surface Water Sampling (1)

Sample Location	Iron	Manganese	Chromium	Silver	Zinc	Lead	Cadmium	Mercury	Arsenic	Selenium	Barium	Copper	Calcium	Nickel	Beryllium	Vanadium	Antimony	Thallium	Cobalt	Tin	Aluminum	Magnesium
1a	0.495	0.150	0.100	0.100	0.100	0.100	0.100	0.001	0.030	0.005	0.100	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
1b	0.530	0.140	0.100	0.100	0.100	0.100	0.100	0.001	0.030	0.005	0.100	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
2	0.355	0.155	0.100	0.100	0.100	0.100	0.100	0.001	0.030	0.005	0.100	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
3	1.810	0.400	0.100	0.100	0.100	0.100	0.100	0.001	0.030	0.005	0.120	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
4	4.850	0.400	0.100	0.100	0.100	0.100	0.100	0.001	0.030	0.005	0.110	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
5	4.140	0.580	0.100	0.100	0.100	0.100	0.100	0.001	0.030	0.005	0.110	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
6	4.600	0.390	0.100	0.100	0.100	0.100	0.100	0.001	0.030	0.005	0.100	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
7	4.435	0.160	0.100	0.100	0.100	0.100	0.100	0.001	0.030	0.005	0.100	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
8	4.370	0.630	0.100	0.100	0.100	0.100	0.100	0.001	0.030	0.005	0.122	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA

Sample Location	pH	BOD	Chloride	Ammonia-N	Sulfate	TDS	TOC
1a	6.96	2.4	27	0.10	23.5	151	7
1b	6.96	2.4	27	0.10	23.5	137	9
2	6.91	2.4	29	0.10	28.0	161	8
3	7.15	2.4	37	2.80	10.0	156	16
4	7.02	2.4	43	2.55	14.5	192	24
5	6.61	2.4	39	0.70	14.5	180	23
6	6.64	3.4	330	0.10	64.5	733	12
7	6.94	2.4	6	0.10	14.5	49	25
8	6.11	4.8	17	0.25	129.0	306	NA

Inorganic Analytical Results of April 1986
Delaware Sand and Gravel RI/FS Surface Water Sampling (1)

Sample Location	Iron	Manganese	Chromium	Silver	Zinc	Lead	Cadmium	Mercury	Arsenic	Selenium	Barium	Copper	Calcium	Nickel	Beryllium	Vanadium	Antimony	Thallium	Cobalt	Tin	Aluminum	Magnesium
1	0.190	0.135	0.015	0.010	0.020	0.010	0.005	0.001	0.010	0.005	NA	0.025	NA	0.040	0.005	0.050	0.060	0.010	0.050	0.040	0.200	5.160
2	0.215	0.120	0.015	0.010	0.020	0.010	0.005	0.001	0.010	0.005	NA	0.025	NA	0.040	0.005	0.050	0.060	0.010	0.050	0.040	0.200	5.220
3	0.390	0.170	0.015	0.010	0.020	0.010	0.005	0.002	0.010	0.005	NA	0.025	NA	0.040	0.005	0.050	0.060	0.010	0.050	0.040	0.200	5.190
4	0.100	0.440	0.015	0.010	0.020	0.010	0.005	0.001	0.010	0.005	NA	0.025	NA	0.040	0.005	0.050	0.060	0.010	0.050	0.040	0.200	5.000
5	0.405	0.545	0.015	0.010	0.020	0.010	0.005	0.001	0.010	0.005	NA	0.025	NA	0.040	0.005	0.050	0.060	0.010	0.050	0.040	0.200	5.000
6	0.100	0.044	0.015	0.010	0.020	0.010	0.005	0.002	0.010	0.005	NA	0.025	NA	0.040	0.005	0.050	0.060	0.010	0.050	0.040	0.200	9.540
7a	0.130	0.015	0.015	0.010	0.020	0.010	0.005	0.001	0.010	0.005	NA	0.025	NA	0.040	0.005	0.050	0.060	0.010	0.050	0.040	0.200	5.000
7b	0.100	0.015	0.015	0.010	0.022	0.010	0.005	0.001	0.010	0.005	NA	0.025	NA	0.040	0.005	0.050	0.060	0.010	0.050	0.040	0.200	5.000
8	3.100	0.610	0.015	0.010	0.115	0.010	0.005	0.001	0.010	0.005	NA	0.025	NA	0.040	0.005	0.050	0.060	0.010	0.050	0.040	0.200	15.160

1. Aray Creek, West of Route 13
2. Aray Creek, East of Route 13, Upstream of Weir
3. Aray Creek, Pond Entrance
4. Aray Creek, Pond Effluent
5. Aray Creek, Under Railroad Bridge
6. Aray Creek, Tidal Gate, East of Route 9
7. Gravel Pit Pond
8. Intermittent Stream East of DS18

a Duplicate analyses
NA Sample not analyzed for this parameter.
(1) Units in ppm except pH (dimensionless).

Table 5.18
Inorganic Analytical Results for Stream Sediments

Inorganic Analytical Results of April 1985 Delaware Sand and Gravel Landfill RI/FS Stream Sediment Sampling (in micrograms per gram) (1)															
Sample Location	pH	Iron	Manganese	Chromium	Silver	Zinc	Lead	Cadmium	Mercury	Arsenic	Selenium	Barium	Copper	Calcium	Nickel
1a	6.96	17,909	167.00	18.19	<10.00	87.27	17.07	<10.00	<0.50	<3.00	<0.50	26.54	NA	NA	NA
1b	6.96	21,902	148.00	15.28	<10.00	28.53	21.40	<10.00	<0.50	<3.00	<0.50	42.80	NA	NA	NA
2	6.91	9,505	190.00	10.21	<10.00	90.92	142.00	<10.00	<0.50	<3.00	<0.50	38.31	NA	NA	NA
3	7.15	44,010	274.00	25.54	<10.00	214.00	175.00	<10.00	<0.50	<3.00	<0.50	79.72	NA	NA	NA
4	7.02	18,510	398.00	<10.00	<10.00	193.00	25.41	<10.00	<0.50	<3.00	<0.50	165.00	NA	NA	NA
5	6.81	45,175	845.00	14.92	<10.00	163.00	70.43	<10.00	<0.50	13.54	<0.50	74.64	NA	NA	NA
6	6.84	27,962	1320.00	14.93	<10.00	240.90	58.73	<10.00	<0.50	<3.00	<0.50	<10.00	NA	NA	NA
7	6.94	2,867	24.26	<10.00	<10.00	22.74	10.11	<10.00	<0.50	<3.00	<0.50	57.34	NA	NA	NA
8	6.11	18,259	87.02	11.57	<10.00	93.04	31.69	<10.00	<0.50	<3.00	<0.50	NA	NA	NA	NA

Inorganic Analytical Results of April 1986
Delaware Sand and Gravel Landfill RI/FS Stream Sediment Sampling
(in micrograms per gram) (1)

Inorganic Analytical Results of April 1986 Delaware Sand and Gravel Landfill RI/FS Stream Sediment Sampling (in micrograms per gram) (1)															
Sample Location	pH	Iron	Manganese	Chromium	Silver	Zinc	Lead	Cadmium	Mercury	Arsenic	Selenium	Barium	Copper	Calcium	Nickel
1	33.7	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	12.26	NA	NA
2	34.2	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	6.56	NA	NA
3	34.0	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	21.23	NA	NA
4	89.9	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	47.92	NA	NA
5	26.9	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	6.35	NA	NA
6	63.3	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	43.15	NA	NA
7a	38.6	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	22.54	NA	NA
7b	27.9	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	13.35	NA	NA
8	58.5	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	0.63	NA	NA

1. Aray Creek, West of Route 13
2. Aray Creek, East of Route 13, Upstream of Weir
3. Aray Creek, Pond Entrance
4. Aray Creek, Pond Effluent
5. Aray Creek, Under Railroad Bridge
6. Aray Creek, Tidal Gate, East of Route 9
7. Gravel Pit Pond
8. Intermittent Stream East of D586

* Duplicate analyses
NA Sample not analyzed for this parameter.
(1) Units in micrograms per gram, except percent moisture (%) and pH (dimensionless).

Table 5.19

DNREC Inorganic Analytical Results of March, 1985
Delaware Sand and Gravel Landfill RI/FS Groundwater Sampling
(milligrams per liter, unless otherwise noted)

Well #	Spec. Cond. (umhos /cm)	pH	Cl	MHA-N	SO4	TDS	TOC	Metals (micrograms per liter)											
								Fe	Mn	Cr	Ag	Zn	Pb	Bi	Cd	Hg	Au	Se	
2a *	2.4	75	5.7	27.5	24.5	85	14	9990	470	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	420
2b *	2.4	73	5.8	12.5	37.0	57	11	10070	505	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	460
23	2.4	54	5.0	10.0	10.0	51	7	<100	<100	<100	<100	<100	<100	NA	<100	<1.0	<30	<5.0	110
24	2.4	85	6.0	10.0	10.0	61	14	<100	<100	<100	<100	<100	<100	NA	<100	<1.0	<30	<5.0	<100
25	2.4	308	5.5	35.0	2.10	161	9	12960	300	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	120
26	2.4	145	5.0	16.5	5.0	84	21	27240	370	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	140
33	2.4	272	6.0	39.5	1.75	145	19	545	<100	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	205
34	3.2	124	5.4	17.5	10.0	74	20	4570	130	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	185
45	2.4	153	5.7	27.0	5.0	99	14	<100	<100	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	165
49	2.4	72	5.8	7.5	5.0	47	13	210	<100	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	120
58 *	2.4	59	6.8	8.0	10.0	43	8	<100	<100	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	<100
59 *	2.4	58	6.7	8.0	10.0	42	7	<100	<100	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	<100
61	2.4	97	5.4	11.5	0.25	66	18	140	<100	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	240
62	2.4	62	5.5	11.0	50.0	78	24	<100	<100	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	140
ANC-2 *	2.4	131	5.7	13.0	10.0	88	19	<100	<100	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	160
ANC-2 *	2.4	134	5.9	14.0	10.0	92	18	<100	<100	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	225
ANC-7	2.4	105	5.6	12.5	10.0	77	55	<100	<100	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	155
ANC-63	2.4	248	5.3	55.0	0.10	143	11	<100	<100	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	200
B-4	2.4	115	6.0	14.0	40.0	73	17	18740	2365	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	450
B-5	2.4	104	5.8	14.0	0.15	72	9	315	<100	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	180
DGC-016	2.4	240	6.6	21.0	2.90	117	27	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
DGC-016	33.0	406	6.5	10.0	0.15	856	42	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
DGC-024	2.4	129	6.8	18.0	14.0	72	13	130	<100	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	<100
DGC-024	31.0	432	6.8	59.0	1.30	285	72	35000	2900	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	<100
DGC-034	2.4	106	6.4	14.0	10.0	66	13	<100	<100	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	<100
DGC-034	74.0	516	6.4	84.0	2.60	398	124	51000	12800	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	450
PH-1	2.4	224	6.5	27.0	0.60	122	24	1770	405	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	150
PH-10	2.4	167	5.9	22.0	1.35	99	24	295	345	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	175
PH-11	2.4	220	6.3	22.0	2.85	118	33	4640	510	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	195
PH-12	2.4	121	5.3	17.0	0.15	80	43	130	105	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	250
PH-13	3.1	123	6.0	15.0	0.10	5.0	19	4310	370	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	120
PH-14 *	2.4	456	6.5	38.0	16.50	196	57	6400	690	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	210
PH-14 *	2.4	448	6.4	40.0	19.50	17.0	189	57	5960	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	280
27	2.4	338	6.3	38.0	7.00	162	45	4880	390	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	255
28	4.0	352	6.5	66.5	9.00	289	63	22620	1210	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	360
29	13.5	978	6.9	102.0	10.50	523	117	37040	2280	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	475
31	7.4	266	6.4	30.0	2.05	170	31	12880	1190	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	265
PH-2 *	2.4	214	8.1	8.0	0.30	73.0	33	235	<100	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	175
PH-2 *	2.4	214	8.3	8.0	0.25	60.0	159	21	260	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	140
PH-1	2.4	182	5.5	38.0	10.0	112	65	205	<100	<100	<100	<100	<100	<100	<100	<1.0	<30	<5.0	125

* Duplicate analyses
NA Sample not analyzed for this parameter.

Table 5.20
DNREC Organic Analytical Results of March 1985
Delaware Sand and Gravel Landfill RI/FS Groundwater Sampling
(micrograms per liter)

Well #	1,2-dichloro ethane	1,1-dichloro ethene	benzene	toluene	ethyl benzene	1,1-dichloro ethane	chloroform	tri chloro ethene	chloro benzene	1,2-dichloro ethene
3a *	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
3a *	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
23	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
24	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
25	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
26	3.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
33	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
34	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
45	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
49	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
58 *	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
58 *	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
61	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
62	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	180.0	<5.0	<5.0
ANC-2 *	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
ANC-2 *	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
ANC-7	11.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
ANC-63	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
B-4	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
B-5	20.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
D6C-01d	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
D6C-01s	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
D6C-02d	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
D6C-02s	23.0	<5.0	3100.0	7300.0	390.0	8.2	<1.0	28.0	14.0	28.0
D6C-03d	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
D6C-03s	93.0	<5.0	1700.0	8000.0	1400.0	11.0	5.0	320.0	33.0	<1.0
RW-1	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
RW-10	51.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
RW-11	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
RW-12	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
RW-13	<5.0	<5.0	30.0	83.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
RW-14 *	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
RW-14 *	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
27	<5.0	5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
28	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
29	<5.0	<5.0	<5.0	16.0	59.0	<5.0	<5.0	<5.0	24.0	<5.0
31	<5.0	<5.0	130.0	360.0	24.0	<5.0	<5.0	<5.0	<5.0	<5.0
PW-2 *	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
PW-2 *	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
TW-1	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0

* Duplicate analyses

Table 5.21
Indicator Parameter Analytical Results of April, 1986
Delaware Sand and Gravel Landfill RI/FS Groundwater Sampling
(milligrams per liter unless otherwise noted)

Well #	Lab	Alkalinity as CaCO3	Hardness	Chloride	Total Nitrogen	Ammonia as N	Sulfate	TSS	TDS	DOC	Specific Cond. (umhos/cm)	DBP Field Measurements				
												pH	Temp. (C)	Dissolved Oxygen (% saturation)	Specific Conductance (umhos/cm)	
3A	DMREC	15.0	18.0	10.6	0.84	0.43	5.00	343.0	101.0	23.3	NA	6.54	13	NA	80	
25 **	DMREC	28.0	28.0	5.8	0.40	<0.10	20.60	55.0	48.0	13.1	NA	7.50	14	NA	79	
25 **	DMREC	28.0	32.0	5.7	0.20	0.14	19.50	42.0	46.0	10.1	NA	NA	NA	NA	NA	
26	DMREC	44.0	36.0	18.1	0.79	0.22	20.00	114.0	94.0	29.7	NA	3.70	12	NA	120	
33	DMREC	4.0	54.0	34.3	0.35	0.23	11.84	29.0	152.0	19.3	NA	6.66	12	NA	150	
34	DMREC	129.0	124.0	32.7	3.56	3.49	13.00	38.0	226.0	49.4	NA	6.70	10	NA	40	
37	DMREC	81.0	80.0	7.5	9.90*	2.63	70.60	3437.0	119.0	24.4	NA	7.70	18	NA	140	
38	DMREC	79.0	64.0	28.8	0.82*	2.52	46.30	120.0	149.0	44.8	NA	7.40	17	NA	300	
40	DMREC	45.0	34.0	13.9	8.20*	8.07	19.80	274.0	93.0	46.9	NA	7.20	19	NA	130	
45 **	DMREC	13.0	42.0	27.1	0.70	0.04	7.90	50.0	138.0	6.2	NA	NA	15	NA	100	
45 **	DMREC	12.0	40.0	27.5	1.03	0.07	8.00	41.0	120.0	6.6	NA	NA	NA	NA	NA	
56 **	DMREC	11.0	44.0	16.0	0.20	0.13	12.90	16.0	88.0	18.1	NA	4.47	17	19.7	100	
56 **	DMREC	12.0	44.0	15.8	0.20	0.10	12.80	17.0	86.0	17.4	NA	NA	NA	NA	NA	
57	DMREC	10.0	20.0	9.0	0.95	0.22	15.00	100.0	61.0	14.2	NA	4.28	19	17.6	58	
58	DMREC	9.0	28.0	7.1	0.30	<0.10	8.60	38.0	52.0	11.9	NA	6.67	22	25.6	70	
61	DMREC	19.0	26.0	12.1	0.61	0.43	10.70	64.0	121.0	15.5	NA	6.20	11	10.0	60	
62 **	DMREC	12.0	18.0	6.0	0.69	0.28	17.50	182.0	199.0	29.0	NA	3.35	10	24.2	40	
62 **	DMREC	11.0	12.0	8.9	0.65	0.38	18.00	180.0	92.0	37.7	NA	NA	NA	NA	NA	
TH-1	DMREC	19.0	30.0	32.3	0.70	0.52	7.90	99.0	138.0	9.2	NA	7.20	10	13.7	100	
TH-4	DMREC	27.0	30.0	10.8	2.12	1.29	14.00	193.0	124.0	8.3	NA	7.70	10	NA	60	
RM-1 **	DMREC	40.0	42.0	23.6	0.60	0.30	10.90	0.0	100.0	53.4	NA	7.20	16	NA	140	
RM-1 **	DMREC	41.0	52.0	23.5	0.60	0.29	11.10	0.0	103.0	24.2	NA	NA	NA	NA	NA	
RM-10	DMREC	24.0	44.0	22.6	1.62	1.58	5.00	1.0	107.0	38.1	NA	6.20	12	NA	115	
RM-11	DMREC	55.0	56.0	24.0	7.80	3.71	6.00	3.0	154.0	35.8	NA	NA	11	NA	150	
RM-12 **	DMREC	110.0	62.0	34.4	3.97*	10.35	18.00	2.0	209.0	50.7	NA	5.90	12	NA	245	
RM-12 **	DMREC	110.0	64.0	34.1	3.92*	10.35	23.00	2.0	170.0	53.1	NA	NA	NA	NA	NA	
RM-13	DMREC	21.0	34.0	16.8	1.28	0.48	8.30	4.0	133.0	25.4	NA	6.30	10	NA	70	
RM-14 **	DMREC	107.0	76.0	27.3	4.00*	11.71	23.00	2.0	163.0	46.5	NA	6.45	11	NA	225	
RM-14 **	DMREC	102.0	98.0	26.6	0.85*	11.93	20.00	0.0	153.0	33.3	NA	NA	NA	NA	NA	
27	DMREC	102.0	54.0	40.7	9.48	9.38	18.00	10.0	185.0	47.6	NA	6.39	10	NA	250	
28 **	DMREC	116.0	70.0	46.2	3.83*	8.37	29.00	15.0	188.0	46.7	NA	NA	12	NA	290	
28 **	DMREC	117.0	68.0	46.4	3.80*	8.20	32.00	12.0	199.0	45.9	NA	NA	NA	NA	NA	
29	DMREC	241.0	116.0	81.0	4.01*	12.94	38.00	19.0	374.0	82.1	NA	7.00	13	NA	500	
31	DMREC	64.0	46.0	23.8	2.16	2.04	23.00	3.0	121.0	39.3	NA	NA	14	NA	205	
31	EA	53.6	50.0	25.0	2.30	1.45	5.00	90.0	5.0	2.4	221	NA	NA	NA	NA	

* These data are unusable due to laboratory quality control violations.

** Duplicate analyses

NA Sample not analyzed for this parameter.

Table 5.21
(CONTINUED)
Indicator Parameter Analytical Results of April, 1986
Delaware Sand and Gravel Landfill RI/FS Groundwater Sampling
(milligrams per liter unless otherwise noted)

Well #	Lab	Alkalinity as CaCO ₃	Hardness	Chloride	Total Nitrogen	Ammonia as N	Sulfate	TSS	TDS	DOC	Specific Cond. (umhos/cm)	DGC Field Measurements				
												pH	Eh (mv)	Temp. (C)	Dissolved Oxygen (% saturation)	Specific Conductance (umhos/cm)
DGC-01d	DWEL	75.0	58.0	10.7	3.11*	3.44	-	82.0	94.0	29.1	NA	6.40	60	14	NA	125
DGC-01s	DWEL	41.0	50.0	20.3	0.49*	0.79	18.00	111.0	2010.0	46.1	NA	5.35	240	12	NA	160
DGC-02d	DWEL	79.0	32.0	12.2	0.45	0.45	18.00	187.0	146.0	12.4	NA	NA	NA	13	NA	125
DGC-02s	DWEL	112.0	90.0	46.4	2.02	1.55	55.00	182.0	275.0	76.4	NA	NA	NA	13	NA	280
DGC-02s	EA	71.2	130.0	45.0	1.50	1.02	13.00	220.0	120.0	42.0	361	NA	NA	10	NA	80
DGC-03d	DWEL	18.0	36.0	12.8	0.35	0.11	6.00	42.0	111.0	28.9	NA	NA	NA	10	NA	420
DGC-03s	DWEL	138.0	146.0	106.5	7.25	4.50	29.00	103.0	457.0	124.0	NA	NA	NA	10	NA	3220
DGC-04	DWEL	140.0	90.0	52.7	3.40	2.30	60.60	205.0	406.0	240.0	NA	NA	NA	10	NA	NA
DGC-04	DWEL	144.0	90.0	52.9	3.38	2.23	50.60	196.0	414.0	241.0	NA	NA	NA	10	NA	NA
DGC-05	DWEL	54.0	56.0	33.4	1.33	1.12	55.40	168.0	125.0	26.1	NA	6.48	-80	16	13.0	210
DGC-06	DWEL	90.0	106.0	63.2	2.75	2.22	29.00	223.0	309.0	86.7	NA	NA	NA	13	NA	300
DGC-06	EA	62.5	140.0	58.0	2.30	1.44	6.00	250.0	190.0	51.3	406	NA	NA	10	NA	85
DGC-07d	DWEL	30.0	34.0	14.5	1.35	0.99	86.00	334.0	104.0	22.7	NA	NA	NA	10	NA	NA
DGC-07d	DWEL	26.0	200.0	15.1	1.62	1.03	86.00	321.0	101.0	21.5	NA	NA	NA	11	NA	530
DGC-07d	DWEL	172.0	174.0	55.3	1.04	0.28	34.00	110.0	375.0	82.6	NA	NA	NA	13	NA	130
DGC-07d	DWEL	168.0	174.0	55.1	1.06	0.26	38.00	69.0	371.0	83.4	NA	6.48	105	11	NA	325
DGC-08d	DWEL	22.0	32.0	14.0	0.62	0.57	-	25.0	74.0	21.2	NA	7.15	-162	11	NA	140
DGC-08s	DWEL	119.0	134.0	57.1	1.60	1.52	29.00	82.0	265.0	59.8	NA	NA	NA	12	NA	14
DGC-09d	DWEL	52.0	54.0	15.4	0.68	0.27	18.00	35.0	141.0	50.5	NA	NA	NA	13	35.0	3250
DGC-09d	DWEL	53.0	56.0	15.7	0.49	0.33	18.00	51.0	152.0	7.8	NA	6.59	157	12	42.0	70
DGC-09s	DWEL	54.0	50.0	29.2	2.06	1.10	23.00	1340.0	124.0	13.8	NA	7.46	99	13	70.1	130
DGC-10d	DWEL	107.0	374.0	14.0	1.08	0.70	47.50	242.0	1566.0	21.7	NA	6.50	-45	12	36.0	145
DGC-10s	DWEL	18.0	26.0	17.3	2.28	1.65	101.10	429.0	145.0	17.8	NA	11.75	71	13	NA	200
DGC-11d	DWEL	87.0	94.0	4.8	1.29	0.47	21.20	110.0	166.0	23.7	NA	6.59	157	12	NA	1325
DGC-11s	DWEL	190.0	112.0	15.1	2.76	2.23	142.50	1068.0	266.0	NA	NA	7.11	79	11	NA	150
DGC-12d	DWEL	32.0	28.0	6.4	0.31	0.68	40.00	169.0	85.0	13.5	NA	NA	NA	14	NA	200
DGC-12s	DWEL	465.0	76.0	58.6	1.72	0.27	6.00	88.0	578.0	12.6	NA	NA	NA	13	NA	1325
DGC-13	DWEL	46.0	84.0	9.8	1.04	0.23	75.00	2426.0	222.0	NA	NA	5.36	154	12	NA	150
DGC-13	EA	60.5	130.0	15.0	0.40	-	72.00	200.0	1100.0	1.9	286	NA	NA	NA	NA	NA
PAUC-2	DWEL	11.0	36.0	11.3	0.39	<10.00	<5.00	2.0	85.0	23.9	NA	NA	NA	14	NA	85
PAUC-7	DWEL	80.0	30.0	12.4	0.39	<0.10	<5.00	0.0	78.0	28.0	NA	NA	NA	13	NA	70
PAUCB-3	DWEL	73.0	38.0	50.4	0.39	<0.10	<5.00	0.0	132.0	18.6	NA	NA	NA	14	NA	150
PAUCB-3	EA	11.8	40.0	49.0	<0.10	<0.01	5.00	100.0	<5.0	<0.3	220	NA	NA	NA	NA	NA
B-4	DWEL	32.0	34.0	19.0	3.00	0.00	26.00	95.0	113.0	35.3	NA	6.09	-37	13	NA	160
B-5	DWEL	24.0	24.0	10.6	0.44	0.40	11.66	76.0	81.0	9.0	NA	7.25	27	12	NA	60

* These data are unusable due to laboratory quality control violations.

** Duplicate analyses

- Non-detectable

NA Sample not analyzed for this parameter.

Table 5.22

Inorganic Analytical Results of April, 1986
Delaware Sand and Gravel Landfill RI/FS Groundwater Sampling
(micrograms per liter)

Method	Lab	Al	Si	As	Ba	Be	Cd	Ca	Cr	Co	Cu	Fe	Pb	Hg	Mn	Hg	Ni	K	Sr	Ag	Na	Tl	Sb	V	Zn
3a	CLP	529	24	10	96	1.0	0.5	1530	3.0	7.0	4.3	4860	5.0	519	223	0.1	6.5	894	5.0	3.0	4870	10	16	5.0	23
2a	CLP	119	26	10	39	0.4	0.5	4030	3.0	7.0	4.3	23400	5.0	2460	234	0.1	7.5	1420	5.0	3.0	9100	10	16	5.0	23
33	CLP	223	26	10	59	0.4	0.5	13000	4.0	6.0	7.9	60	5.0	4750	85	0.1	14.0	2730	5.0	3.0	20900	10	16	5.0	72
45	CLP	119	26	10	56	1.0	0.5	9710	3.0	7.0	5.0	3400	5.0	3400	57	0.1	6.0	2370	5.0	3.0	9600	10	16	5.0	34
54	CLP	223	26	10	17	0.4	0.5	5230	4.0	6.0	7.1	50	5.0	1440	27	0.1	8.7	3700	5.0	3.0	4320	10	16	5.0	74
61	CLP	223	26	10	31	0.4	0.5	4570	4.0	7.7	5.4	275	5.0	2300	148	0.1	7.6	2060	5.0	3.0	5720	10	16	5.0	55
62	CLP	223	26	10	19	0.4	0.5	3940	4.0	9.2	4.4	30	5.0	788	64	0.1	13.0	1900	5.0	3.0	4670	10	16	5.0	62
MEC-2	CLP	119	26	10	61	1.0	0.5	7700	3.0	7.0	9.8	48	5.0	3890	5.7	0.1	6.0	1580	5.0	3.0	6770	10	16	5.0	9.2
MEC-7	CLP	119	26	10	54	1.0	0.5	6400	3.0	7.0	8.4	48	5.0	2980	4.0	0.1	6.0	1310	5.0	3.0	5740	10	16	5.0	11
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0.5	8100	3.0	7.0	23	46	11.0	3400	5.6	0.1	6.0	1380	5.0	3.0	23100	10	16	5.0	14
MEC-83	EA	70	25	10	72	1.0	0																		

Organic Analytical Results of April, 1986
Delaware Sand and Gravel Landfill RI/FS Groundwater Sampling
(micrograms per liter)

Well #	Lab	Acetone	1,1-dichloro ethane	2-butanone (MEK)	1,2-dichloro ethane	ethyl benzene	total xylenes	bis (2-ethyl phthalate benzene)	bis (2-chloro ethyl) ether	tri chloro ethane (TCE)	viny chloride	4-ethyl pentanone (HEK)	2-methyl phenol (o-cresol)
34	CLP	6 WJ	5	9 WJ	5	5	5	3 WJ	5	5	5	5	5
35	CLP	15 WJ	5	13 WJ	5	5	5	10	5	5	5	5	5
36	CLP	8 WJ	5	11 WJ	5	5	5	8 WJ	5	5	5	5	5
37	CLP	11 WJ	5	10 WJ	5	5	5	9 WJ	5	5	5	5	5
38	CLP	10 WJ	5	6 WJ	5	5	5	17 WJ	5	5	5	5	5
39	CLP	10 WJ	5	11 WJ	5	5	5	6 WJ	5	5	5	5	5
40	CLP	7 WJ	5	10 WJ	5	5	5	23 WJ	5	5	5	5	5
41	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
42	CLP	7 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
43	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
44	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
45	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
46	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
47	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
48	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
49	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
50	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
51	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
52	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
53	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
54	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
55	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
56	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
57	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
58	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
59	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
60	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
61	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
62	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
63	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
64	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
65	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
66	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
67	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
68	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
69	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
70	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
71	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
72	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
73	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
74	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
75	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
76	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
77	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
78	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
79	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
80	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
81	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
82	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
83	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
84	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
85	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
86	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
87	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
88	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
89	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
90	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
91	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
92	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
93	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
94	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
95	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
96	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
97	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
98	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
99	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
100	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
101	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
102	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
103	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
104	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
105	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
106	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
107	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
108	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
109	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
110	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
111	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
112	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
113	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
114	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
115	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
116	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
117	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
118	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
119	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
120	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
121	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
122	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
123	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
124	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
125	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
126	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
127	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
128	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
129	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
130	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
131	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
132	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
133	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
134	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
135	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
136	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
137	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
138	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
139	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
140	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
141	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
142	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
143	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
144	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
145	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
146	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
147	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
148	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
149	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
150	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
151	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
152	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
153	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
154	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
155	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
156	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
157	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
158	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
159	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
160	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5	5	5	5
161	CLP	6 WJ	5	10 WJ	5	5	5	5	5	5			

- Analytical data is not available.

Enlightened executives recognize that quality control criteria were not set.

1. **Identify the problem.** The first step in the problem-solving process is to identify the problem. This involves recognizing the issue and understanding its scope and impact.

1980-1981

Table 5.23 (cont'd)
Organic Analytical Results of April, 1986
Delaware Sand and Gravel Landfill RI/FS Groundwater Sampling
(micrograms per liter)

Well #	Lab	di-n butyl phthalate	1,2- dichloro ethane	1,4- dichloro benzene	styrene	ethyl phenol (p-cresol)	benzoic acid	naph- thalene	diethyl phthalate	phenol	1,2- dichloro benzene	chloro- form	tetra- chloro ethene (PCE)	2,4- dichloro phenol
3a	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
26	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
33	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
45	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
50	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
61	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
62	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
AWC-2	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
AWC-7	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
AWC-81 *	EA	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2
AWC-83 *	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
AWC-83 *	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
B-4	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
B-5	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
B6C-01d	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
B6C-01s	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
B6C-02d	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
B6C-02s	EA	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2
B6C-03d	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
B6C-03s	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
B6C-04 *	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
B6C-04 *	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
B6C-04 *	EA	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2
B6C-07d	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
B6C-07s	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
B6C-08d	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
B6C-08s	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
B6C-09d	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
B6C-09s	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
B6C-09s	EA	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2
B6C-10d	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
B6C-10s	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
B6C-11d	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
B6C-11s	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
B6C-12d	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
B6C-12s	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
B6C-13 *	EA	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2
B6C-13 *	EA	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2
RN-10 *	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
RN-10 *	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
RN-11	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
RN-12	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
RN-13	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
RN-14	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
27	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
28	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
29	CLP	<10	<5	<5	<5	<10	<50	<10	<10	<10	<10	<5	<5	<10
31 *	EA	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2
31 *	EA	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2	<2

* Duplicate analyses
- Analytical data is not available.
J Estimated quantity because quality control criteria were not met.

Appendix B

Analytical Data of Soils at Delaware Sand and Gravel Landfill

Table 5.10
Inorganic Analytical Results of the April, 1985
Delaware Sand and Gravel Landfill RI/FS Surface Soil Sampling
(in micrograms per gram)

Soil Sample #	Fe	Mn	Cr	Ag	In	Pb	Cd	Hg	As	Se	Ba	Cu	Ca	Ni	Be	V	Sb	Te	Co	Sn	Al	Mg
S1	67,449	550	23.98	<10	67.86	29.08	<10	<0.40	4.08	<0.50	121.00	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
S2	10,828	224	13.73	<10	20.36	10.89	<10	<0.40	<3.00	<0.50	53.50	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
S3*	28,342	300	15.32	<10	44.06	33.52	<10	<0.40	<3.00	<0.50	73.28	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
S3*	22,634	307	13.89	<10	51.72	26.69	<10	<0.40	<3.00	<0.50	73.75	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
S4	30,880	466	18.72	<10	43.52	20.75	<10	<0.40	<3.00	<0.50	96.66	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
S5	14,314	354	13.31	<10	31.56	22.68	<10	<0.40	<3.00	<0.50	69.53	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
S6	36,388	693	20.62	<10	63.38	41.25	<10	<0.40	<3.00	<0.50	108.00	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
S7	37,223	412	19.98	<10	60.94	24.98	<10	<0.40	<3.00	<0.50	103.00	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
S8	56,573	290	23.81	<10	63.14	40.89	<10	<0.40	3.73	<0.50	110.00	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
S9	18,824	251	13.89	<10	28.77	23.81	<10	<0.40	<3.00	<0.50	88.29	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
S10	14,176	151	10.66	<10	22.29	14.53	<10	<0.40	<3.00	<0.50	36.82	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
S11	19,405	349	10.30	<10	24.34	16.38	<10	<0.40	<3.00	<0.50	41.67	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
S12	15,656	598	11.11	<10	78.89	17.68	<10	<0.40	<3.00	<0.50	45.45	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
S13	62,546	139	<10.00	<10	16.48	<10.00	<10	<0.40	<3.00	<0.50	21.48	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
S14	7,659	123	<10.00	<10	39.65	67.69	<10	<0.40	3.09	<0.50	12.57	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
S15	11,616	380	11.18	<10	42.17	35.06	<10	<0.40	3.76	<0.50	88.92	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA

* Duplicate analyses were performed on this sample. The results presented are the highest between the duplicates.
NA Sample not analyzed for this parameter.

Table 5.11
Inorganic Analytical Results of April, 1986
Delaware Sand and Gravel Landfill RI/FS Surface Soil Sampling
(milligrams per kilogram)

Sample #	Percent Moisture	Al	Sb	As	Ba	Be	Ca	Cr	Co	Cu	Fe	Pb	Hg	Mn	Hg	K	Se	Ag	Na	Tl	Sn	V	Zn
B-01	10.0	2070	14	35.6	23.0	0.82	478	15.0	3.9	23.3	8300	50.3	0.056	13.0	301	2.8	2.8	1.7	363	3.6	8.9	11.0	50.3
B-01a	24.0	4070	17	64.6	8.8	0.44	232	6.9	210	24	2460	8.6	0.130	8.3	337	3.3	3.3	2.0	430	6.6	11.0	3.9	62.0
B-01b	24.0	3190	17	64.6	9.3	0.44	232	11.0	214	48	6660	12.3	0.160	9.7	357	3.3	3.3	2.0	430	6.6	11.0	3.3	62.0
B-02a	16.0	2210	15	44.0	34.0	0.40	130	27.0	30	76	37000	19.3	0.071	28.0	743	30.0	1.8	1.8	389	48.0	9.5	5.1	32.0
B-02b	18.0	8280	16	4.1	86.0	0.48	130	44.0	478	50	27000	60.3	0.056	2.700	20.0	180	3.0	1.8	389	48.0	9.5	5.1	32.0
B-03a	22.0	8640	17	64.6	86.0	0.44	232	138.0	82.3	304.3	21900	100.3	0.130	32.0	443	3.2	1.9	1.9	419	6.6	14.3	41.0	104.3
B-03b	20.0	2260	16	64.3	42.0	0.58	232	38.0	245	131.3	21900	55.3	0.130	8.0	458	3.1	2.1	1.8	408	6.3	10.0	14.0	57.3
B-03c	14.0	447	15	35.8	26.0	0.38	232	20.0	351.3	73.3	21700	14.3	0.058	3.4	315	2.9	1.8	390	43.0	9.3	3.1	11.3	
B-03d	36.0	277	20	77.8	18.0	0.78	232	11.0	260.3	519.3	27500	70.3	0.058	7.1	423	3.9	2.3	430	43.0	12.0	3.9	5.1	
B-03e	26.0	12300	18	12.0	82.0	1.70	43.4	1580	45.0	37.3	24300	19.3	0.048	24.0	1410	3.4	2.0	441	6.8	11.0	36.0	117.3	
B-03f	6.0	3790	14	65.3	48.0	0.53	232	1150	24.0	57.3	22800	54	1.280	13.0	449	2.7	1.6	605.3	43.3	8.5	17.0	117.3	
B-04a	16.0	11900	15	64.0	43.0	1.00	43.0	749	24.0	5.4	18300	14.3	0.060	9.6	500	3.0	2.1	477.3	48.0	9.5	35.0	30.3	
B-04b	14.0	9250	15	64.0	54.8	1.30	43.0	446	22.0	8.2	18300	14.3	0.060	6.5	411	3.0	2.7	678.3	48.0	9.5	32.0	23.1	
B-04c	12.0	24	15	53.7	40.0	0.37	232	200	9.2	15.3	2870	12.3	0.200	3.4	308	2.8	1.7	331	43.7	9.1	12.8	4.8	
B-04d	6.0	1480	14	53.3	58.0	1.00	232	31.4	33.0	15.3	28000	31.3	1.020	12.0	404	2.7	1.6	560.3	43.3	8.5	8.9	25.3	
B-05a	14.0	2410	15	53.8	18.0	0.38	232	309	4.0	4.1	5850	5.7	0.058	3.9	315	2.9	1.7	380	3.8	9.3	17.0	31.0	
B-05b	18.0	6200	16	64.1	40.0	0.41	232	1210	11.0	4.3	13600	110	0.061	10.0	377	3.0	1.8	398	48.1	4.8	30.0	50.0	
B-05c	13.0	8590	15	53.9	45.0	0.39	232	207	11.0	12	13500	7.1	0.059	7.8	319	2.9	1.8	384	43.9	9.4	29.0	21.0	
B-05d	13.0	3520	15	53.7	19.0	0.37	232	202	4.7	4.0	8040	11.3	0.057	5.0	312	2.9	1.7	375	43.7	9.2	19.0	17.0	
B-05e	20.0	4800	16	64.3	33.0	0.43	232	255	8.5	4.4	8590	8.1	0.063	4.9	339	3.1	1.9	408	46.3	10.0	22.0	16.0	
B-05f	24.0	9340	17	7.9	47.0	1.00	43.3	745	13.0	10	18200	25.3	0.066	11.0	456	3.3	2.0	430	46.6	11.0	38.0	34.0	
B-05g	20.0	10500	16	64.3	52.0	0.94	43.1	245	14.0	8.6	16900	7.5	0.063	13.0	384	3.1	1.9	408	46.3	10.0	39.0	35.0	
B-05h	18.0	4000	16	64.1	45.0	0.41	232	324	9.7	7.3	22900	9.6	0.064	6.8	330	3.0	1.8	398	48.1	9.8	24.0	18.0	
B-05i	22.0	11200	17	64.4	45.0	0.41	232	344	11.0	6.5	22900	9.6	0.064	10.0	402	3.2	1.9	398	48.1	9.8	24.0	18.0	
B-05j	18.0	7110	16	64.1	34.0	0.34	232	116	4.4	3.9	14200	11.3	0.061	7.2	349	3.0	1.8	398	48.1	9.8	24.0	18.0	
B-05k	10.0	4850	14	53.6	47.0	0.51	232	196	4.4	4.3	9790	9.4	0.056	4.7	301	2.8	1.7	383	43.6	8.9	16.0	23.0	
B-06	NA	10200	89	16.0	8020.0	0.43	232	10300	222.0	23.3	123000	4750	0.062	158.0	776	3.1	3.7	889.3	46.3	116.3	44.0	4380.3	
B-07	20.0	8920	122	92.0	4450.0	0.79	29.0	2100	158.0	8.3	44000	3400	0.075	125.0	569	3.1	1.9	1140	66.3	279	93.0	309	
B-08	39.0	12700	16	27.0	183.0	0.89	43.1	3560	24.0	8.9	32800	420	0.062	19.0	1210	3.1	1.9	403	66.2	19.0	52.0	40.0	
B-09a	28.0	10800	18	64.9	58.0	0.79	43.3	976	16.0	7.1	17900	13.3	0.069	13.0	438	3.5	2.1	453	66.9	11.0	40.0	41.0	
B-09b	32.0	4340	19	67.4	55.0	0.74	43.7	1090	13.0	7.1	15400	9.6	0.074	12.0	399	3.7	2.2	480	67.4	12.0	33.0	41.0	
B-09c	31.0	10700	19	67.2	75.0	1.40	43.6	546	19.0	11	23000	29.3	0.072	11.0	481	3.6	2.2	473	67.2	12.0	52.0	39.0	
B-09d	18.0	15200	16	64.7	44.0	1.40	43.0	245	17.0	9.1	19300	9.8	0.061	13.0	570	3.0	1.8	398	48.1	9.8	42.0	28.0	
B-09e	20.0	13700	16	64.3	48.0	1.40	43.1	282	17.0	10	22100	10.3	0.063	12.0	540	3.1	1.9	403	66.3	10.0	43.0	34.0	
B-09f	12.0	14400	16	64.1	70.0	1.20	43.1	220	22.0	5.1	27400	20.3	0.063	14.0	472	3.1	2.3	408	66.3	10.0	50.0	32.0	
B-09g	13.0	4180	25	53.7	29.0	0.54	232	1190	7.7	6.1	10800	10.3	0.057	6.1	312	2.9	1.7	375	43.7	9.2	19.0	26.0	
B-09h	14.0	3270	15	53.8	28.0	0.58	232	402	8.8	5.0	8880	12.3	0.058	5.1	315	2.9	1.7	380	43.8	9.3	19.0	19.0	
B-09i	12.0	7370	15	53.7	37.0	0.67	232	200	11.0	4.0	17800	6.2	0.057	5.7	308	28.0	1.7	371	43.7	9.1	24.0	15.0	
B-09j	37.0	344	239	82.0	121.0	0.82	43.1	1090	11.0	8.4	17000	172	1.500	13.0	870	41.0	2.5	1690.3	82.0	13.0	44.1	1.6	
B-10	12.0	9970	16	64.0	41.0	0.93	43.0	212	14.0	8.7	14900	6.6	0.072	10.0	387	3.0	1.8	393	46.0	9.6	32.0	23.0	
B-11	19.0	14400	16	64.2	88.0	1.40	43.1	237	18.0	8.9	22800	9.3	0.062	12.0	526	3.1	1.9	403	66.2	9.9	47.0	31.0	
B-12	20.0	14600	16	6.2	89.0	1.40	43.1	261	19.0	9.4	24500	18.3	0.063	13.0	480	3.1	1.9	408	66.3	10.0	55.0	32.0	

s.d. suffix implies 0-1' sampling interval; 'd' suffix implies 2-3' sampling interval; no designation implies single sample at location from 0-1'

a. Duplicate analyses

j. Estimated quantity because quality control criteria were not met

NA Sample not analyzed for this parameter.

Table 5.12

Organic Analytical Results of April, 1986
Delaware Sand and Gravel Landfill RI/FS Surface Soil Sampling
(micrograms per kilograms)

Sample Site	Moisture	Percent Chloride	Methylene Chloride	Acetone	2-butanone (MEK)	tri-chloro-ethene	4-methyl-2-pentanone (MIBK)	2-hexanone	tetra-chloro-ethene	Toluene	Ethyl Benzene	Total Naphthalene	di-benzo-furan	phen-anthrene	di-n-butyl-phthalate
0-1	0	0	2 UU	10	10	10	10	10	10	10	10	10	10	10	10
B-01	0	0	2 UU	10	10	10	10	10	10	10	10	10	10	10	10
B-01a	32	7	4 UU	25 UU	14	15	43	15	46	120	6	90	29000	29000	29000
B-01b	20	5 UU	5 J	21 UU	14	13	13	13	13	6	6	6	25000	25000	25000
B-02a	22	1 UU	23 JM	55 UU	11	11	11	11	11	20	6	11	26000	26000	26000
B-03a	17	1 UU	19 UU	19 UU	12	12	12	12	12	6	6	6	21000	21000	21000
B-03b	22	6 UU	21 UU	21 UU	13	13	13	13	13	6	6	6	24000	24000	24000
B-04a	13	5 UU	23 UU	23 UU	11	11	11	11	11	6	6	6	26000	26000	26000
B-04b	29	3 UU	180 UU	14	14	14	14	14	14	7	7	7	23000	23000	23000
B-05a	20	3 UU	15 UU	14	14	14	14	14	14	7	7	7	140000	140000	140000
B-05b	11	2 UU	11	11	11	11	11	11	11	6	6	6	460	460	460
B-06a	14	2 UU	15 UU	12	12	12	12	12	12	6	6	6	370	370	370
B-06b	3.21	2 UU	11	11	11	11	11	11	11	6	6	6	390	390	390
B-07a	10	3 UU	12 UU	11	11	11	11	11	11	6	6	6	410	410	410
B-07b	6	2 UU	13 UU	11	11	11	11	11	11	6	6	6	370	370	370
B-07c	6	2 UU	13 UU	11	11	11	11	11	11	6	6	6	350	350	350
B-08a	15	1 UU	9 UU	12	12	12	12	12	12	6	6	6	390	390	390
B-08b	15	4 UU	9 UU	12	12	12	12	12	12	6	6	6	390	390	390
B-09a	18	2 UU	12	12	12	12	12	12	12	6	6	6	410	410	410
B-09b	16	1 UU	12	12	12	12	12	12	12	6	6	6	400	400	400
B-09c	25	5 UU	13	13	13	13	13	13	13	7	7	7	440	440	440
B-09d	23	6 UU	13	13	13	13	13	13	13	6	6	6	430	430	430
B-09e	21	1 UU	13	13	13	13	13	13	13	6	6	6	420	420	420
B-09f	25	1 UU	13	13	13	13	13	13	13	6	6	6	440	440	440
B-09g	12	1 UU	11	11	11	11	11	11	11	6	6	6	380	380	380
B-09h	21	4 UU	13	13	13	13	13	13	13	6	6	6	420	420	420
B-09i	10	2 UU	11	11	11	11	11	11	11	6	6	6	370	370	370
B-09j	9	2 UU	11	11	11	11	11	11	11	6	6	6	370	370	370
B-09k	10	2 UU	11	11	11	11	11	11	11	6	6	6	370	370	370
B-09l	38	3 UU	15 UU	16	16	16	16	16	16	8	8	8	340	340	340
B-09m	36	2 UU	16 UU	16	16	16	16	16	16	8	8	8	320	320	320
B-09n	29	1 UU	46 UU	46	46	46	46	46	46	7	7	7	470	470	470
B-10	18	2 UU	12	12	12	12	12	12	12	6	6	6	410	410	410
B-11	24	1 UU	13	13	13	13	13	13	13	6	6	6	440	440	440
B-12	21	3 UU	13	13	13	13	13	13	13	6	6	6	420	420	420
B-13a	10	1 UU	11	11	11	11	11	11	11	6	6	6	370	370	370
B-13b	10	2 UU	11	11	11	11	11	11	11	6	6	6	370	370	370
B-13c	16	1 UU	12	12	12	12	12	12	12	6	6	6	400	400	400
B-14a	7	2 UU	11	11	11	11	11	11	11	6	6	6	370	370	370
B-14b	10	2 UU	11	11	11	11	11	11	11	6	6	6	370	370	370
B-15	10	2 UU	11	11	11	11	11	11	11	6	6	6	370	370	370
B-16	10	2 UU	11	11	11	11	11	11	11	6	6	6	370	370	370
B-17	10	1 UU	11	11	11	11	11	11	11	6	6	6	370	370	370

5,6 's' suffix implies 0-1' sampling interval; 'd' suffix implies 2-3' sampling interval; no designation implies single sample at location from 0-1'.

9 Duplicate analyses

J Estimated quantity because quality control criteria were not met

M Tentative identification

UU A compound was detected but not in high enough concentrations to confirm its presence.

Delaware Sand and Gravel Landfill RI/FS Surface Soil Sampling (micrograms per kilogram)

Sample Site	Fluor- anthene	Pyrene	butyl- benzyl- phthalate	bis (2-ethyl- hexyl)- phthalate	beta- BHC	gamma- BHC	hepta- chlor- epoxide	methoxy- chlor	PCB- 1254	PCB- 1260	Phenol	benzo(a) pyrene	dichloro benzene
													trichloro isoeer ethane
B-01	29000	29000	29000	17000 J	250	250	480 R	2500	4900	4900	29000	29000	122 J
B-01a	25000	25000	25000	12500 J	422	130 R	140 R	420	430	430	25000	25000	7
B-02a	28000	28000	28000	28000	850	850	1850	1850	17000	17000	26000	26000	5
B-02b	21000	21000	21000	21000	1180	34 R	180	1800	3500	3500	21000	21000	43 J
B-03a	27000	27000	27000	87000	780	780	780	7600	16000	16000	24000	24000	6
B-03b	27000	27000	27000	27000	210	210	2100	4100	4100	4100	26000	26000	6
B-04a	23000	23000	23000	23000	1190	1190	1190	11900	3760	3760	23000	23000	6
B-04b	140000	140000	140000	140000	140	140	1400	2800	2800	2800	140000	140000	7
B-05a	46	46	46	46	230	230	2300	2300	4700	4700	460	460	7
B-05b	370	370	370	300	37	37	37	370	750	750	370	370	6
B-05c	390	390	390	390	339	339	339	339	78	78	390	390	6
B-06a	410	410	410	410	41	41	41	81	81	81	410	410	6
B-07a	370	370	370	370	37	37	37	370	740	740	370	370	6
B-07b	350	350	350	350	18	18	18	180	350	350	350	350	5
B-01a	390	390	390	390	339	339	339	339	78	78	390	390	6
B-01b	390	390	390	390	339	339	339	339	78	78	390	390	6
B-02a	410	410	410	410	41	41	41	81	81	81	410	410	6
B-02b	400	400	400	400	40	40	40	40	79	79	400	400	6
B-03a	440	440	440	440	44	44	44	89	89	89	440	440	6
B-03b	430	430	430	430	43	43	43	87	87	87	430	430	6
B-04a	420	420	420	420	42	42	42	84	84	84	420	420	6
B-04b	440	440	440	440	44	44	44	89	89	89	440	440	6
B-05a	380	380	380	380	38	38	38	38	76	76	380	380	6
B-05b	420	420	420	420	42	42	42	84	84	84	420	420	6
B-06	370	370	370	370	37	37	37	37	74	74	370	370	6
B-07 a	110 J	1400	330 J	330 J	37	37	37	370	1500	1500	50 J	50 J	66 J
B-07 b	370	370	370	180	337	337	337	337	220 J	220 J	34 J	34 J	370
B-08	370	370	370	370	337	337	337	337	74	74	370	370	6
B-09 a	340	340	340	340	34	34	34	34	110	110	340	340	6
B-09 b	350	350	350	350	352	352	352	352	150	150	350	350	13 J
B-09c	470	470	470	470	47	47	47	47	94	94	470	470	6
B-10	410	410	410	410	41	41	41	81	81	81	410	410	6
B-11	440	440	440	440	44	44	44	89	89	89	440	440	6
B-12	420	420	420	420	42	42	42	84	84	84	420	420	6
B-13a	370	370	370	370	37	37	37	37	74	74	370	370	6
B-13b	370	370	370	370	37	37	37	37	74	74	370	370	6
B-14a	400	400	400	400	40	40	40	40	79	79	400	400	6
B-14b	18000	18000	18000	18000	720	720	720	7200	49000	49000	18000	18000	2 J
B-15	370	370	370	370	37	37	37	37	74	74	370	370	6
B-16	370	370	370	370	37	37	37	37	74	74	370	370	6
B-17	370	370	370	370	37	37	37	37	74	74	370	370	6

NA Sample not analyzed for this compound.

Table 5.15
Inorganic Analytical Results of February/March, 1986
Delaware Sand and Gravel Landfill RI/FS Soil Boring Sampling
(milligrams per kilogram)

Well #	Depth (ft)	Zone Sampled	% Moisture	Al	Sb	As	Ba	Be	Cd	Ca	Cr	Co	Cu	Fe	Pb	Hg	Mn	Ni	K	Se	Ag	Na	Tl	Sr	V	Zn		
DEC-04	5-4	6-8	C	33.5	48700	38	8.8	146	2.6	3.0	720	36.0	22	12	48900	6.8	984	121	24	474	3.0	5.3	2030	4.5	20	101	42	
DEC-04	5-7	12-14	C	40.1	33400	42	18.0	116	2.5	3.3	808	30.0	31	13	53900	18.0	1060	38	28	532	3.3	5.8	2250	3.0	23	71	39	
DEC-04	5-10	18-20	C	14.6	7030	29	4.7	339	1.8	2.2	330	15.0	12	13	28100	4.1	289	86	11	293	2.2	3.9	1510	3.5	16	23	10	
DEC-04	5-12	23-27	C	10.3	3300	28	4.5	337	1.7	2.2	333	4.8	11	8.4	11900	4.7	188	33	11	279	2.2	3.9	1510	3.3	15	17	9.5	
DEC-04	5-13	30-32	C	13.5	8320	29	4.6	339	1.7	2.3	346	7.1	12	9.2	14700	2.9	133	130	12	289	2.2	4.0	1560	3.5	16	17	18	
DEC-04	5-14	35-47	UPCC	18.8	10400	31	4.9	441	1.8	2.5	500	6.6	12	9.9	2270	8.0	247	8.7	10	310	2.5	4.3	1660	3.7	17	18	10	
DEC-04	5-17	50-52	UPCC	14.8	2120	29	4.7	339	2.3	2.3	691	69.0	12	39	11800	7.0	240	42	13	569	2.3	4.1	1580	3.5	16	92	18	
DEC-04	5-17	50-52	UPCC	15.4	1390	30	4.7	440	1.8	2.4	762	20.0	12	28	3910	7.1	237	17	12	398	2.4	4.1	1600	3.5	16	37	10	
DEC-05	5-2	5-7	C	14.2	3470	29	4.7	339	1.7	2.3	348	6.5	12	9.3	20400	2.9	181	121	12	291	2.3	4.1	1570	3.5	16	17	10	
DEC-05	5-3	10-12	C	12.3	2500	29	4.6	338	1.7	2.3	341	9.0	11	9.1	19800	2.3	136	38	11	285	2.3	4.0	1540	3.4	15	17	9.7	
DEC-05	5-3	10-12	C	12.8	2540	29	4.6	338	1.7	2.3	343	6.2	11	9.2	23300	1.7	136	81	11	287	2.3	4.0	1550	3.4	15	17	9.7	
DEC-05	5-4	15-17	C	13.8	2310	29	4.6	339	1.7	2.3	347	6.6	12	9.3	8680	2.3	169	40	11	290	2.3	4.1	1570	3.5	16	17	9.9	
DEC-05	5-4	40-42	UPCC	15.2	898	29	4.7	440	1.9	2.4	353	8.6	12	16	4900	2.4	140	26	12	295	2.4	4.1	1590	3.5	16	22	10	
DEC-06	5-5	8-10	C	16.1	11600	30	8.9	49	1.8	2.4	356	18.0	12	9.3	18800	8.9	677	173	12	298	2.4	4.2	1610	3.6	16	28	26	
DEC-06	5-7	12-14	C	15.2	5070	29	5.3	440	1.8	2.4	353	14.0	12	9.4	10400	4.7	166	62	14	295	2.4	4.1	1590	3.5	16	18	10	
DEC-06	5-10	18-20	C	14.7	3990	29	4.7	339	1.8	2.3	351	27.0	12	9.4	22600	3.5	322	341	11	293	2.3	4.1	1580	3.5	16	25	17	
DEC-06	5-12	25-27	C	17.8	7230	30	4.9	441	1.8	2.4	364	14.0	12	9.7	24900	6.7	628	269	13	402	2.4	4.3	1640	3.6	16	33	31	
DEC-06	5-13	30-32	C/UPCC	11.2	1550	28	4.5	338	1.7	2.3	393	9.3	11	11	9730	3.9	177	41	11	282	2.3	3.9	1520	3.4	15	32	9.6	
DEC-06	5-17	50-52	UPCC	19.5	353	31	5.0	442	1.9	2.5	371	5.0	12	10	3530	1.9	148	129	12	311	2.5	4.3	1680	3.7	17	19	11	
DEC-06	5-18	55-57	UPCC	19.3	1090	31	5.0	442	1.9	2.5	371	12.0	12	11	6900	1.9	147	892	12	310	2.5	4.3	1670	3.7	17	19	11	
DEC-07	5-4	15-17	C	32.6	34100	37	12.0	95	2.2	3.0	545	44.0	15	12	23000	15.0	1050	332	24	442	3.0	5.2	2000	4.5	20	86	43	
DEC-07	5-5	20-22	C	13.5	3180	29	4.6	339	1.7	2.3	346	4.6	12	9.2	12400	2.3	240	88	11	289	2.3	4.0	1560	3.5	16	17	11	
DEC-07	5-7	30-32	C	17.7	6430	30	4.9	441	1.8	2.4	363	11.0	12	18	52100	3.6	291	52	16	304	2.4	4.3	1640	3.6	16	18	27	
DEC-07	5-13	70-72	UPCC	30.5	603	34	5.8	448	2.2	2.9	430	5.8	14	12	2030	2.9	171	24	14	360	2.9	5.0	1940	4.3	19	22	12	
DEC-07	5-15	70-72	UPCC	19.5	234	31	5.0	442	1.9	2.5	371	1.9	12	9.9	816	1.2	148	12	12	310	2.5	4.3	1680	3.7	17	19	11	
DEC-08	5-2	5-7	C	37.1	53100	41	16.0	137	2.8	3.6	585	37.0	24	12	47300	19.0	1270	646	26	785	2.0	5.0	184	4.4	49	77	44	
DEC-08	5-3	10-12	C	34.2	84400	41	15.0	135	2.7	3.5	302	38.0	26	11	47500	16.0	1500	742	33	956	1.9	5.0	147	4.4	51	51	51	
DEC-08	5-4	15-17	C	16.3	1840	32	3.2	20	2.1	3.0	91	1.6	8.4	4	5180	1.6	181	278	11	9.4	188	2.2	4.8	179	1.8	8.4	9	
DEC-08	5-4	15-17	C	12.9	3160	32	3.3	23	2.0	4.0	167	1.5	8.0	4.9	8020	1.5	333	172	11	9.2	520	2.1	4.8	156	1.7	16	8.4	
DEC-08	5-10	45-47	UPCC	17.2	639	32	3.3	14	2.1	4.0	180	1.7	8.5	5.2	310	1.6	41	1.3	9.7	479	2.2	4.8	115	1.8	1.8	1.8	1.8	
DEC-09	5-2	5-7	C	19.0	20700	43	3.3	67	2.2	3.2	644	25.0	9.2	5.3	25300	9.3	2220	248	17	1890	2.3	5.0	150	4.4	19	43	29	
DEC-09	5-3	10-12	C	15.0	21400	42	3.2	72	2.1	3.1	617	17.0	8.2	7.6	22200	7.6	1650	108	15	1300	2.2	5.0	135	4.4	18	38	26	
DEC-09	5-5	20-22	C	14.3	4870	42	3.2	21	2.0	3.9	756	1.5	8.2	5.0	6170	3.3	209	30	10.1	9.3	347	2.2	5.0	256	4.4	18	9.9	5.3
DEC-09	5-18	85-87	UPCC	21.8	281	43	3.5	34	2.2	3.2	181	1.3	9.0	5.0	2730	5.7	18	1.8	10	192	2.4	5.0	143	4.4	18	7.0	8.4	
DEC-13	5-1	0-2	C	6.0	7590	-	5.1	76	-	-	563	9.5	-	-	8120	14.0	762	573	-	-	-	-	-	5.5	1.3	-	17	
DEC-13	5-2	5-7	C	3.0	11300	-	11.0	44	-	-	878	18.0	-	-	9.1	10400	8.8	34	-	-	977	-	-	5.5	1.3	-	19	
DEC-17	5-2	20-22	C	2.0	2880	-	1.8	1	-	-	61	15.0	-	-	9.8	11100	6.7	1850	108	-	-	-	-	5.9	1.3	-	-	
DEC-17	5-4	35-37	C	9.0	11900	-	6.7	59	-	-	545	15.0	-	-	-	-	-	-	16	1420	-	-	-	7.3	1.3	-	41	

* Duplicate analyses
 - Non-detectable; Detection limits not specified.
 UJ A compound was detected but not in high enough concentrations to confirm its presence.
 J Estimated quantity because quality control criteria were not met

C Columbia Formation
 UPCC Upper Potomac confining clay
 uJP upper Upper Potomac Hydrologic Zone

Table

Organic Analytical Results of February/March 1986
Delaware Sand and Gravel Landfill RI/FS Soil Boring Sampling
(micrograms per kilogram)

Well Number	Sample Number	Depth (ft)	Zone Sampled	Percent Moisture (%)	Toluene	Methylene Chloride	Acetone	2-butanone (MEK)	4-ethyl-2-pentanone (NIBK)	Ethyl Benzene	Total Xylene	1,2-dichloroethane	1,1,1-trichloroethane	Phenol	bis-(2-chloroethyl) ether	4-methylphenol	41-n-butyl phthalate	bis-(2-ethylhexyl) phthalate	benzoic acid	benzoanthracene
SEC-04	S-1	0-2	C	31.0	0.0	7.0 W	14 W	14	14	14	14	14	14	14	14	14	14	14	14	14
SEC-04	S-2	2-4	C	33.7	0.0	8.0 W	14 W	14	14	14	14	14	14	14	14	14	14	14	14	14
SEC-04	S-3	4-6	C	26.1	0.0	7.0 W	14 W	14	14	14	14	14	14	14	14	14	14	14	14	14
SEC-04	S-4	6-8	C	32.9	0.0	7.0 W	23 W	14	14	14	14	14	14	14	14	14	14	14	14	14
SEC-04	S-5	8-10	C	31.0	0.0	7.0 W	23 W	14	14	14	14	14	14	14	14	14	14	14	14	14
SEC-04	S-6	10-12	C	32.6	0.0	7.0 W	24 W	14	14	14	14	14	14	14	14	14	14	14	14	14
SEC-04	S-7	12-14	C	28.5	0.0	8.0 W	24 W	14	14	14	14	14	14	14	14	14	14	14	14	14
SEC-04	S-8	14-16	C	31.9	0.0	7.0 W	14 W	14	14	14	14	14	14	14	14	14	14	14	14	14
SEC-04	S-9	16-18	C	29.4	0.0	7.0 W	14 W	14	14	14	14	14	14	14	14	14	14	14	14	14
SEC-04	S-10	18-20	C	8.5	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-11	20-22	C	2.39	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-12	22-24	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-13	30-32	C	13.4	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-14	32-34	C	14.0	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-15	34-36	C	14.0	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-16	36-38	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-17	38-40	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-18	40-42	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-19	42-44	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-20	44-46	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-21	46-48	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-22	48-50	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-23	50-52	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-24	52-54	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-25	54-56	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-26	56-58	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-27	58-60	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-28	60-62	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-29	62-64	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-30	64-66	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-31	66-68	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-32	68-70	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-33	70-72	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-34	72-74	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-35	74-76	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-36	76-78	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-37	78-80	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-38	80-82	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-39	82-84	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-40	84-86	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-41	86-88	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-42	88-90	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-43	90-92	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-44	92-94	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-45	94-96	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-46	96-98	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-47	98-100	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-48	100-102	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-49	102-104	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-50	104-106	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-51	106-108	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-52	108-110	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-53	110-112	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-54	112-114	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-55	114-116	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-56	116-118	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-57	118-120	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-58	120-122	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-59	122-124	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-60	124-126	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-61	126-128	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-62	128-130	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-63	130-132	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-64	132-134	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-65	134-136	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-66	136-138	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-67	138-140	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-68	140-142	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-69	142-144	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-70	144-146	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-71	146-148	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-72	148-150	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-73	150-152	C	14.2	0.0	5.0 W	11 W	11	11	11	11	11	11	11	11	11	11	11	11	11
SEC-04	S-74	152-154	C	14.2	0.0	5.0 W	11 W	11	11											

Table (continued)
Organic Analytical Results of February/March 1986
Delaware Sand and Gravel Landfill RI/FS Soil Boring Sampling
(micrograms per kilogram)

Well Number	Sample Number	Depth (ft)	Zone Sampled	Percent Moisture (%)	Toluene	Methylene Chloride	Acetone	2-butanone (MEK)	4-ethyl-2-pentanone (HEK)	Total Ethyl Benzene	1,2-dichloro ethane	1,1,1-trichloro ethane	Phenol	bis-(2-chloro ethyl) ether	4-ethyl phenol	di-n-butyl phthalate	bis-(2-ethyl hexyl) phthalate	Naphthalene	benzoic acid	benzo anthracene
MEC-07	5-1	0-2	C	25.2	7.0	7.0	13 W	13	13	7.0	7.0	7.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-2	5-7	C	31.8	7.0	7.0	24 W	15	15	7.0	7.0	7.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-3	10-12	C	25.5	7.0	7.0	30 W	13	13	7.0	7.0	7.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-4	15-17	C	33.3	7.0	7.0	42 W	15	15	7.0	7.0	7.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-5	20-22	C	14.5	6.0	6.0	34 W	12	12	6.0	6.0	6.0	180	620	620	4900 W	480 W	480	3700	480
MEC-07	5-6	25-27	C	14.1	6.0	6.0	12 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-7	30-32	C	16.9	6.0	6.0	20 W	12	12	6.0	6.0	6.0	350	350	350	900 W	500 W	350	2400	350
MEC-07	5-8	35-37	C	11.5	6.0	6.0	11 W	11	11	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-9	40-42	UPCC	13.6	6.0	6.0	12 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-10	45-47	UPCC	17.8	6.0	6.0	12 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-11	50-52	UPCC	19.2	6.0	6.0	22 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-12	55-57	UPCC	28.5	6.0	6.0	10 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-13	60-62	UPCC	28.6	6.0	6.0	17 W	13	13	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-14	65-67	UPCC	28.1	6.0	6.0	970	350	46	13	13	13	320	320	320	1000 W	570 W	320	2400	320
MEC-07	5-15	70-72	UPCC	17.4	6.0	6.0	1100	910	61	30	30	30	350	350	350	1100 W	550	350	2400	350
MEC-07	5-16	75-77	UPCC	21.9	6.0	6.0	7.0 W	15	15	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-17	80-82	UPCC	12.5	6.0	6.0	6.0 W	11	11	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-18	85-87	UPCC	16.3	6.0	6.0	6.0 W	11	11	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-19	90-92	UPCC	17.9	6.0	6.0	7.0 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-20	95-97	UPCC	19.5	6.0	6.0	12 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-21	100-102	UPCC	18.4	6.0	6.0	12 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-22	105-107	UPCC	18.4	6.0	6.0	11 W	11	11	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-23	110-112	UPCC	19.1	6.0	6.0	6.0 W	11	11	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-24	115-117	UPCC	13.9	6.0	6.0	23 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-25	120-122	UPCC	15.4	6.0	6.0	6.0 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-26	125-127	UPCC	19.0	6.0	6.0	6.0 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-27	130-132	UPCC	16.4	6.0	6.0	6.0 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-28	135-137	UPCC	11.7	6.0	6.0	6.0 W	11	11	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-29	140-142	UPCC	10.9	6.0	6.0	6.0 W	11	11	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-07	5-30	145-147	UPCC	17.4	6.0	6.0	6.0 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-1	0-2	C	28.0	6.0	6.0	13 W	14	14	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-2	5-7	C	34.0	6.0	6.0	21 W	14	14	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-3	10-12	C	34.0	6.0	6.0	23 W	15	15	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-4	15-17	C	29.0	6.0	6.0	13 W	14	14	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-5	20-22	C	11.0	6.0	6.0	8.7 W	11	11	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-6	25-27	C	15.0	6.0	6.0	7.0 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-7	30-32	UPCC	12.0	6.0	6.0	14 W	11	11	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-8	35-37	UPCC	18.0	6.0	6.0	20 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-9	40-42	UPCC	19.0	6.0	6.0	9.8 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-10	45-47	UPCC	19.0	6.0	6.0	1.1 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-11	50-52	UPCC	17.0	6.0	6.0	1.1 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-12	55-57	UPCC	17.0	6.0	6.0	1.1 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-13	60-62	UPCC	19.0	6.0	6.0	22 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-14	65-67	UPCC	29.0	6.0	6.0	7.3 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-15	70-72	UPCC	17.0	6.0	6.0	3.9 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-16	75-77	UPCC	17.0	6.0	6.0	13 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-17	80-82	UPCC	26.0	6.0	6.0	16 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-18	85-87	UPCC	16.0	6.0	6.0	8.8 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-19	90-92	UPCC	15.0	6.0	6.0	4.7 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-20	95-97	UPCC	16.0	6.0	6.0	9.0 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-21	100-102	UPCC	18.0	6.0	6.0	10 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-22	105-107	UPCC	20.0	6.0	6.0	20 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-23	110-112	UPCC	22.0	6.0	6.0	13 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-24	115-117	UPCC	14.0	6.0	6.0	33 W	14	14	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-25	120-122	UPCC	15.0	6.0	6.0	13 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-26	125-127	UPCC	13.0	6.0	6.0	10 W	11	11	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA
MEC-08	5-27	130-132	UPCC	16.0	6.0	6.0	10 W	12	12	6.0	6.0	6.0	NA	NA	NA	NA	NA	NA	NA	NA

Duplicate analyses
Sample not analyzed for this compound.
N Tentative identification
A compound was detected but not in high enough concentrations to confirm its presence.
EJ quantity because quality control criteria were not met.

C Columbia Formation
UPCC Upper Potomac confining clay
WUP upper Potomac Hydrologic Zone
UPCC upper Potomac Hydrologic Zone
WUP upper Potomac Hydrologic Zone
WUP upper Potomac Hydrologic Zone
WUP upper Potomac Hydrologic Zone

Table (continued)
Organic Analytical Results of February/March 1986
Delaware Sand and Gravel Landfill RI/FS Soil Boring Sampling
(micrograms per kilogram)

Well Number	Sample Number	Depth (ft)	Zone Sampled	Percent Moisture (%)	Toluene	Methylene Chloride	Acetone	2-butanone (MEK)	4-methyl-2-pentanone (MIBK)	Ethyl Benzene	Total Tylene	1,2-dichloro ethane	1,1,1-trichloro ethane	Phenol	bis-(2-chloro ethyl) ether	4-ethyl phenol	di-n-butyl phthalate	bis-(2-ethyl hexyl) phthalate	Methylphenyl ketone	benzoic acid	anthracene
MEC-09	S-1	0-2	C	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0
MEC-09	S-2	3-7	C	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0
MEC-09	S-3	10-12	C	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0
MEC-09	S-4	15-17	C	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0
MEC-09	S-5	20-22	C	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0
MEC-09	S-6	25-27	C	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0
MEC-09	S-7	30-32	UPCC	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0
MEC-09	S-8	35-37	UPCC	14.0	14.0	14.0	14.0	14.0	14.0	14.0	14.0	14.0	14.0	14.0	14.0	14.0	14.0	14.0	14.0	14.0	14.0
MEC-09	S-9	40-42	UPCC	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0
MEC-09	S-10	45-47	UPCC	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0
MEC-09	S-11	50-52	UPCC	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0
MEC-09	S-12	55-57	UPCC	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0
MEC-09	S-13	60-62	UPCC	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0
MEC-09	S-14	65-67	UPCC	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0
MEC-09	S-15	70-72	UPCC	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0
MEC-09	S-16	75-77	UPCC	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0
MEC-09	S-17	80-82	UP	21.0	21.0	21.0	21.0	21.0	21.0	21.0	21.0	21.0	21.0	21.0	21.0	21.0	21.0	21.0	21.0	21.0	21.0
MEC-09	S-18	85-87	UP	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0
MEC-09	S-19	90-92	UP	21.0	21.0	21.0	21.0	21.0	21.0	21.0	21.0	21.0	21.0	21.0	21.0	21.0	21.0	21.0	21.0	21.0	21.0
MEC-09	S-20	95-97	UP	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0	13.0
MEC-09	S-21	100-102	UP	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0
MEC-09	S-22	105-107	UP	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0
MEC-09	S-23	110-112	UP	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0
MEC-09	S-24	115-117	UP	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0
MEC-09	S-25	120-122	UP	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0
MEC-09	S-26	125-127	UP	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0
MEC-09	S-27	130-132	UP	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0	18.0
MEC-09	S-28	135-137	UP	22.0	22.0	22.0	22.0	22.0	22.0	22.0	22.0	22.0	22.0	22.0	22.0	22.0	22.0	22.0	22.0	22.0	22.0
MEC-09	S-29	140-142	UP	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0	19.0
MEC-09	S-30	145-147	UP	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0
MEC-09	S-31	150-152	UP	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0
MEC-09	S-32	155-157	UP	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0	12.0
MEC-09	S-33	160-162	UP	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0
MEC-09	S-34	165-167	UP	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0
MEC-13	S-1	0-2	C	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0
MEC-13	S-2	3-7	C	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0	17.0
MEC-13	S-3	10-12	C	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0	15.0
MEC-15	S-1	5-7	C	18.5	18.5	18.5	18.5	18.5	18.5	18.5	18.5	18.5	18.5	18.5	18.5	18.5	18.5	18.5	18.5	18.5	18.5
MEC-15	S-2	13-15	C	11.4	11.4	11.4	11.4	11.4	11.4	11.4	11.4	11.4	11.4	11.4	11.4	11.4	11.4	11.4	11.4	11.4	11.4
MEC-15	S-3	21-23	C	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4
MEC-16	S-1	13-15	C	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4	15.4
MEC-16	S-2	21-23	C	9.44	9.44	9.44	9.44	9.44	9.44	9.44	9.44	9.44	9.44	9.44	9.44	9.44	9.44	9.44	9.44	9.44	9.44
MEC-16	S-3	29-31	C	11.9	11.9	11.9	11.9	11.9	11.9	11.9	11.9	11.9	11.9	11.9	11.9	11.9	11.9	11.9	11.9	11.9	11.9
MEC-17	S-1	20-22	C	10.0	10.0	10.0	10.0	10.0	10.0	10.0	10.0	10.0	10.0	10.0	10.0	10.0	10.0	10.0	10.0	10.0	10.0
MEC-17	S-2	30-32	C	14.0	14.0	14.0	14.0	14.0	14.0	14.0	14.0	14.0	14.0	14.0	14.0	14.0	14.0	14.0	14.0	14.0	14.0
MEC-17	S-3	35-37	C	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0	20.0

a Duplicate analyses
 NA Sample not analyzed for this compound.
 H Tentative identification
 UJ This compound was detected but not in high enough concentrations to confirm its presence.
 P Estimated quantity because quality control criteria were not met.
 Preliminary: Blank contamination precludes confirmation of compound presence or quantity.

C Columbia Formation
 UPCC Upper Potomac confining clay
 UJ Upper Upper Potomac Hydrologic Zone
 UPCC Upper Potomac dividing clay
 UJ Lower Upper Potomac Hydrologic Zone
 MFC Middle Potomac clay