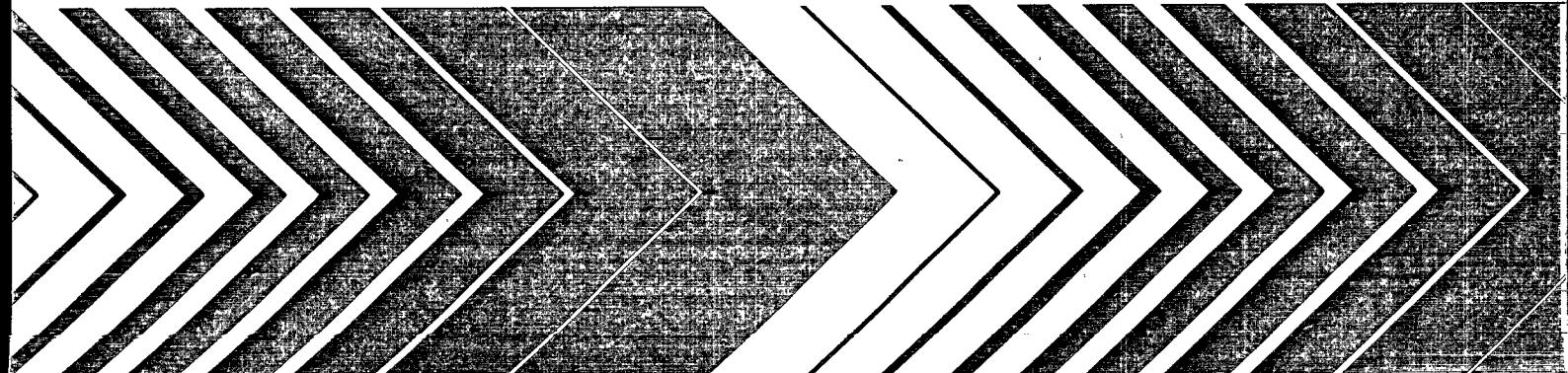

Research and Development



Estimating Water Treatment Costs

Volume 4 Computer User's Manual for Retrieving and Updating Cost Data



RESEARCH REPORTING SERIES

Research reports of the Office of Research and Development, U.S. Environmental Protection Agency, have been grouped into nine series. These nine broad categories were established to facilitate further development and application of environmental technology. Elimination of traditional grouping was consciously planned to foster technology transfer and a maximum interface in related fields. The nine series are:

1. Environmental Health Effects Research
2. Environmental Protection Technology
3. Ecological Research
4. Environmental Monitoring
5. Socioeconomic Environmental Studies
6. Scientific and Technical Assessment Reports (STAR)
7. Interagency Energy-Environment Research and Development
8. "Special" Reports
9. Miscellaneous Reports

This report has been assigned to the ENVIRONMENTAL PROTECTION TECHNOLOGY series. This series describes research performed to develop and demonstrate instrumentation, equipment, and methodology to repair or prevent environmental degradation from point and non-point sources of pollution. This work provides the new or improved technology required for the control and treatment of pollution sources to meet environmental quality standards.

This document is available to the public through the National Technical Information Service, Springfield, Virginia 22161.

ESTIMATING WATER TREATMENT COSTS

Volume 4. Computer User's Manual for
Retrieving and Updating Cost Data

by

Thomas S. Lineck
Robert C. Gumerman
Russell L. Culp

Culp/Wesner/Culp
Consulting Engineers
Santa Ana, California 92707

Contract No. 68-03-2516

Project Officer

Robert M. Clark
Drinking Water Research Division
Municipal Environmental Research Laboratory
Cincinnati, Ohio 45268

MUNICIPAL ENVIRONMENTAL RESEARCH LABORATORY
OFFICE OF RESEARCH AND DEVELOPMENT
U.S. ENVIRONMENTAL PROTECTION AGENCY
CINCINNATI, OHIO 45268

DISCLAIMER

This report has been reviewed by the Municipal Environmental Research Laboratory, U.S. Environmental Protection Agency, and approved for publication. Approval does not signify that the contents necessarily reflect the views and policies of the U.S. Environmental Protection Agency, nor does mention of trade names or commercial products constitute endorsement or recommendation for use.

FOREWORD

The U.S. Environmental Protection Agency (EPA) was created because of increasing public and government concern about the dangers of pollution to the health and welfare of the American people. Noxious air, foul water, and spoiled land are tragic testimonies to the deterioration of our natural environment. The complexity of that environment and the interplay of its components require a concentrated and integrated attack on the problem.

Research and development is that necessary first step in problem solution, and it involves defining the problem, measuring its impact, and searching for solutions. The Municipal Environmental Research Laboratory develops new and improved technology and systems to prevent, treat, and manage wastewater and solid and hazardous water pollutant discharges from municipal and community sources to preserve and treat public drinking water supplies, and to minimize the adverse economic, social, health, and aesthetic effects of pollution. This publication is one of the products of that research--a most vital communications link between the researcher and the user community.

The cost of water treatment processes that may be used by water supply systems to remove contaminants included in the National Interim Primary Drinking Water Regulations is of interest to the EPA, State and local agencies, and consulting engineers. This volume contains documentation and user information for the WATER program, a FORTRAN computer program that retrieves and updates cost information for the 72 large-system unit processes and the 27 small system processes presented in Volumes 1, 2, and 3 of this report. The WATER program is capable of determining costs for individual processes and complete treatment plants.

Francis T. Mayo
Director
Municipal Environmental Research
Laboratory

ABSTRACT

This volume is the fourth in a series of four reports on estimating costs for water treatment as a function of system size and treatment efficiency. Volume 4 is a computer users manual and contains a FORTRAN computer program, WATER, that can be used for retrieval and updating of all cost data contained in the Volumes 1, 2 and 3. Volume 1 is the summary volume and discusses the cost estimating approaches utilized to develop the cost curves and the treatment techniques applicable for contaminant removal. It also presents a series of examples demonstrating the use of the cost curves applicable to large water supply systems with treatment capacities between 1 and 200 mgd. Information is included on virus and asbestos removal. Volume 2 presents cost curves for large water systems (1 to 200 mgd), and Volume 3 presents cost curves for small systems (2,500 gpd to 1 mgd).

The WATER program determines costs by retrieving stored coefficients for a least squares polynomial fit of the cost curves presented in Volumes 1, 2, and 3, and by evaluating the polynomial expression for the desired process design parameter. Cost information is presented for construction and operation and maintenance, including energy, maintenance material and labor. The conceptual designs and assumptions used in formulating the cost information are presented in Volumes 1, 2, and 3.

The program will compute costs for individual processes or for a series of processes. Capital costs are determined from construction costs by applying cost factors (input by the user) for engineering, sitework, sub-surface considerations, land, and standby power. The program computes general contractor overhead and profit, legal, fiscal, and administrative fees, and interest during construction based on the overall cost of the project.

All construction costs are stored in terms of October 1978 dollars, and are updated by one of two methods, determined by the user. The program computes a weighted composite cost index for each process, using eight individual cost indices for excavation and sitework, manufactured equipment, concrete, steel, labor, pipe and valves, electrical equipment and instrumentation, and housing - or the user may specify updating by use of the Engineering News Record Construction Cost Index. Operation and maintenance costs are determined from unit costs (input by the user) such as dollars per hour for labor and dollars per kilowatt hour for electricity. Maintenance material costs are stored as dollars per year and are updated using the Bureau of Labor Statistics Price Index.

The user need not be an experienced programmer, but a familiarity with programming is recommended. This report was submitted in fulfillment of Contract No. 68-03-2516 by Culp/Wesner/Culp under the sponsorship of the U.S. Environmental Protection Agency. This report covers the period November 1, 1976 to January 1, 1979. It was completed as of July 2, 1979.

CONTENTS

Foreword	iii
Abstract	iv
Figures	vi
Tables	vi
Acknowledgements	vii
1. Introduction	1
2. Input Data Files	3
3. COST.DAT File Construction	6
4. PROCES.DAT File Construction	9
5. Program Output	34
6. Examples	36
7. Trouble Shooting Guide	57
8. WATER Program Listing	58
9. CRV.DAT File	70

FIGURES

<u>Number</u>		<u>Page</u>
1	PROCES.DAT Data Segments	17
2	Land Requirements for Conventional Plants	18
3	Land Requirements for Package Complete Treatment Plants	19

TABLES

<u>Number</u>		<u>Page</u>
1	COST.DAT File Example	4
2	PROCES.DAT File Example	5
3	Card-by-Card Explanation of COST.DAT File	6
4	Process Cost Curves for Large and Small Water Treatment Systems	10
5	Processes That Use Chemicals and Chemicals Used	15
6	Process Parameter Units	22

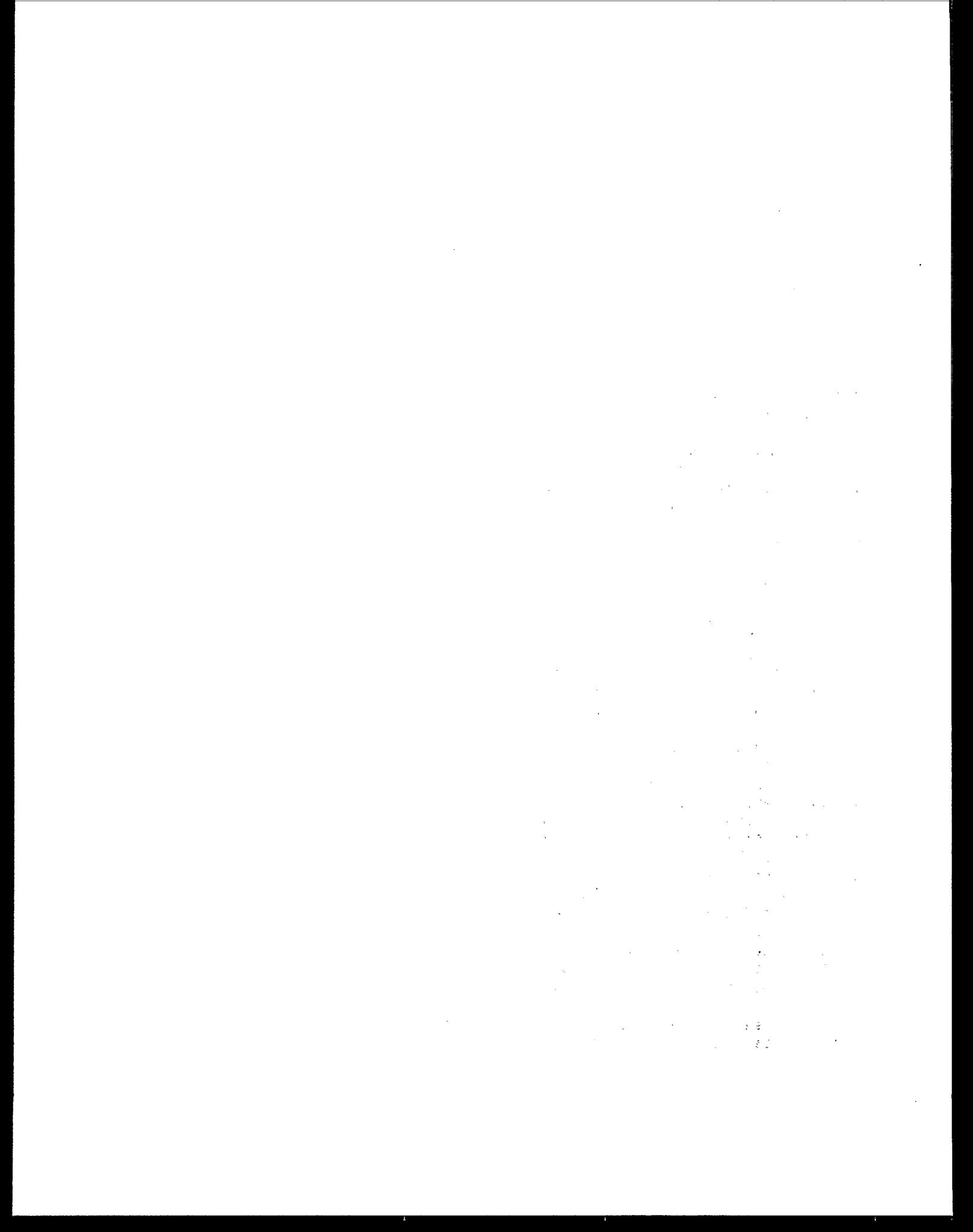
ACKNOWLEDGEMENTS

This report was prepared under the direction of Dr. Robert M. Clark, Municipal Environmental Research Laboratory, Office of Research and Development. The report was prepared by Robert C. Gumerman, Russell L. Culp, Sigurd P. Hansen, Thomas S. Lineck, and Bruce E. Burris of Culp/Wesner/Culp. Ms. Karin J. Wells of Culp/Wesner/Culp was responsible for typing of the final report.

Mr. Ronald M. Dahman of Zurheide-Herrmann, Inc., was responsible for checking all unit costs. Dr. Isadore Nusbaum and Mr. Dean Owens were respective sub-consultants on the reverse osmosis and ion exchange curves.

Special acknowledgement is given to Mr. Keith Carswell, Dr. Robert M. Clark, Mr. Jack De Marco, Dr. Gary Logsdon, Dr. O. Thomas Love, Mr. Benjamin Lykins, Jr., Mr. Thomas J. Sorg, all of the EPA Municipal Environmental Research Laboratory, who reviewed the final report, and Mr. Paul Dorsey, also of the EPA Municipal Environmental Research Laboratory, who reviewed the computer program.

Mrs. Anne Hamilton was the technical editor for all four volumes of this report.



SECTION 1

INTRODUCTION

SCOPE

This report is Volume 4 of a four-volume study that presents construction and operation and maintenance cost curves for 99 unit processes that are especially applicable (either individually or in combination) to the removal of contaminants listed in the National Interim Primary Drinking Water Regulations. This volume is a computer users manual and contains documentation and user information for the WATER program, which is a FORTRAN computer program that retrieves and updates cost information for the 72 large and 27 small water supply systems presented in Volumes 1, 2, and 3 of this report. Costs are also determined for treatment plants, and they are input to the program as trains of individual processes.

BACKGROUND

The WATER program described here can be used as a valuable tool to facilitate retrieval and updating of the cost information presented in Volumes 1, 2, and 3 of this report. Since WATER has been designed to compute costs for entire treatment plants, cost determinations for competing treatment trains or regional variations in operating costs for a particular treatment train can be made quickly and accurately.

The costs generated by this program are broken down into capital costs and operation and maintenance costs. Capital costs include those for construction, engineering, sitework and interface piping, subsurface considerations, standby power, legal, fiscal and administrative services, interest during construction, and land. Operation and maintenance costs include those for electricity, labor, maintenance materials, diesel fuel, natural gas, and chemicals. Most costs are stored as coefficients of third-degree polynomial expressions determined by the method of least squares for the values in the cost tables presented in Volumes 1, 2, and 3. Therefore, the cost generated for a specific point in these tables could vary by as much as 10 to 15 percent from the value generated by the program, depending on the deviation of the values in the table from a smooth curve fit. In general, the differences between the costs generated by the program and the costs obtained through use of the cost curves in Volumes 1, 2, and 3, will be insignificant.

The user need not be an experienced programmer, but a familiarity with programming is recommended.

PURPOSE AND OBJECTIVES

The purpose of this volume is to present complete documentation and user information for the FORTRAN computer program, WATER, which retrieves and updates cost information for the large and small water supply treatment processes presented in Volumes 1, 2, and 3 of this report. The WATER program has been designed to facilitate the estimation of overall treatment plant costs as well as individual process costs.

SECTION 2

INPUT DATA FILES

Three data files are necessary to run this program. Two of these files, COST.DAT and PROCES.DAT, are set up by the user. The third data file, CRV.DAT, is a construction and operation and maintenance data base containing information about each of the water treatment processes considered in this report. This file is an integral part of the program and must be established on the computing system with the main program. Once it is established, the general user should have no need to access the main program, WATER, or the data base, CRV.DAT.

The first of the two data files to be constructed by the user is the COST.DAT file. Table 1 is an example listing of the COST.DAT file. This file basically contains all the cost information necessary to run the program. The variables in this file, called cost factors, must be input in the sequence shown in Table 1. A detailed explanation of the input format is given in the following section on COST.DAT File Construction.

The second file to be constructed by the user is the PROCES.DAT file. Table 2 is an example listing of the PROCES.DAT file. This file contains information about each of the water treatment processes for which the user desires costs. A detailed explanation of the input format is given in a following section entitled, PROCES.DAT File Construction.

Table 1
COST.DAT File Example

COSTS PRESENTED ARE CURRENT AS OF OCTOBER 1978
CAPITAL COST FACTORS (% OF CONSTRUCTION COST):
1 ENGINEERING(%) =10.
2 SITWORK, INTERFACE PIPING(%) =5.
3 SUBSURFACE CONSIDERATIONS(%) =0.0
4 STANDBY POWER(%) =0.0
5 INTEREST RATE(%) =7.
6 NUMBER OF YEARS =20.0
7 LAND COST, \$/ACRE =2000.
UNIT COST FACTORS:
8 ELECTRICITY, \$/KWH =.03
9 LABOR, \$/HR =10.
10 DIESEL FUEL, \$/GAL =.45
11 NATURAL GAS, \$/CU FT =.0013
12 BLDNG ENERGY USE,KWH/SQ FT/YR =102.6
COST INDEXES:
13 EXCAVATION(ENR SKILLED LABOR) =247.0
14 MANUFACTURED EQUIP (BLS #114) =221.3
15 CONCRETE (BLS #132) =221.1
16 STEEL (BLS #101.3) =262.1
17 LABOR (ENR SKILLED LABOR) =247.0
18 PIPE & VALVES (BLS #114.901) =236.4
19 ELECTRICAL & INSTR (BLS #117) =167.5
20 HOUSING (ENR BUILDING COST) =254.76
21 PRODUCER PRICE INDEX =199.7
22 ENR CONSTRUCTION, '67 BASE YR =0.0
OUTPUT(6 FOR LP,5 FOR TELETYPE) =5
PRINTOUT(DETAILED OR SUMMARY) =SUMMARY
9,2
7.5,12.5

Table 2
PROCES.DAT File Example

SECTION 3
COST.DAT FILE CONSTRUCTION

To aid in understanding the format of this data file, the user is referred to Table 1, which must be constructed as shown. Cards 2, 10, and 16 are for user information only and are skipped by the program when reading this file. They must not be omitted, however, or the program will skip actual data. A card-by-card explanation of this file is given in Table 3.

Table 3
Card-by-Card Explanation of COST.DAT File

<u>Card No.</u>	<u>Explanation</u>
1	First 48 characters printed "as is" on the program output. Intended to be used to denote valid data of cost information produced.
2	For user information only. This line is skipped by the program.
3-9	Capital cost factors as shown. Program read skips the first 34 characters then reads floating point number input. These values must start in Column 35 and must contain a decimal point. Percentage values, as indicated, must be percentages, not decimal values. Example: Engineering must be listed as 10.0 for 10 percent, not as 0.10. The program internally divides by 100.
10	For user information only - skipped by program read.
11-15	Unit cost factors as shown. As with lines 3-9, program read skips the first 34 characters. Values must begin in Column 35 and must contain decimal points. Units are as shown in Table 1.
16	For user information only - skipped by program read.

Card No.Explanation (continued)

- 17-26 Cost indices as shown. As with lines 3-9 and 11-15, program read skips the first 34 characters. Values must begin in Column 35 and must contain decimal points. These cost indices are used to update the cost data base stored in the CRV.DAT file. The user has the option of using the first eight cost indices listed (Excavation through Housing) to update the construction costs produced by the program, or he can use the ENR Construction Cost Index (line 26) in lieu of the first eight indices. The computer will use the ENR Construction Cost Index if the value input is greater than zero. If the value input for the ENR Construction Cost Index is equal to zero, the computer will use the first eight indices.
- 27 This card designates the location for program output. On most computer installations, a "5" designates the teletype or remote terminal. The program output is 132 characters wide, so it is suggested that the line printer be used if the teletype does not have the capacity to print 132 characters per line. The value for this variable must be an integer and must begin in Column 35.
- 28 This card designates a detailed or summary output. See sections 5 (Program Output) and 6 (Examples) for an explanation and sample of these options.
- 29-30 These cards are optional. The user may wish to run the program while varying only one of the cost factors in the COST.DAT file. Cost factors are numbered 1 through 22 for convenience. For example, cost factor number 9 is labor (\$/hr). Thus if the user wants to determine the change in overall operations and maintenance cost based on the regional variation of the cost of electricity across the nation, he first inputs in card 29 the number of the cost factor and the additional number of values to be used for that cost factor. In this case, cards 29 and 30 are as follows for two additional values of cost factor number 9:

Card 29: 9,2
Card 30: 7.5,12.5

Card 30 contains the two additional values of labor (\$/hr) namely, 7.5 and 12.5.

Note that all input values begin in column one for lines 29 and 30, and that they are separated by a comma.

Up to 10 additional values may be input. They must be floating point numbers with decimal points, but they can appear in any column as long as they are separated by a comma.

Card No.

Explanation (continued)

29-30
continued

Cards 29 and 30 shown in the listing of the COST.DAT file in Table 1 accomplish the following: The program computes all costs with the cost of labor (\$/hr) at 10. Then the program is automatically rerun twice with the cost of labor (\$/hr) at 7.5 and 12.5. This produces three complete printouts.

If the user wants to run the program only once, without varying any of the 22 cost factors, cards 29 and 30 are omitted, and the designation of DETAILED or SUMMARY printout is the last card of the COST.DAT file.

SECTION 4

PROCES.DAT FILE CONSTRUCTION

The PROCES.DAT file contains design and operating information about each of the processes for which the user may desire costs. Table 4 lists the processes for which costs are available and includes the process parameter range over which cost information is stored in the computer. For example, process 1 CL2 FEED - CYLINDER STORAGE, has cost information stored in the program data file over a range of 10 to 10,000 lb/day of chlorine feed. Also shown in Table 4 are the number of chemicals used in the treatment process, the process type and the number of data cards.

Chemical cost information is input along with process design and operating parameters, as explained later. The number of chemicals used in the process is listed in Table 4, and in most cases, the types of chemicals used will be obvious (for example, chlorine is used in process 1, CL2 FEED - CYLINDER STORAGE). For convenience, however, Table 5 lists the processes that use chemicals and the chemicals used.

The Process Type listed in Table 4 denotes the way in which information is input to the computer, and the number of data cards indicates the number of cards necessary to input information for that process. There are a total of 11 process types. The input data for each type are described later in this section.

Since the computer program is designed to determine individual process costs and plant costs by totaling the process costs, the PROCES.DAT file is assembled into what is here termed loosely as "segments" of data (Figure 1).

THE ACRES= CARD

Each data segment corresponds to a treatment plant and must begin with the ACRES= card. This card denotes the land area, in acres, required for the plant. If land costs are not to be included, the card should read ACRES=0.0, with the "A" in acres beginning in Column 1. For convenience, typical land area requirements are shown in Figures 2 and 3.

PROCESS DATA CARDS

Following the ACRES= card, data cards for the processes in the plant are assembled sequentially. There may be as many processes as desired, in any order, and processes may be input more than once. The set of process data cards preceded by the ACRES= card constitutes a segment of data (Figure 1).

Table 4
Process Cost Curves for Large and Small Water Treatment Systems

TREATMENT PROCESS - LARGE SYSTEMS	PARAMETER RANGE			NUMBER OF CHEMICALS	PROCESS TYPE	NO. DATA CARDS	
1 CL2 FEED-CYLINDER STORAGE	10.0	TO	10000.0	LB/DAY	1	1	3
2 CL2 FEED-ON SITE STORAGE TANK	2000.0	TO	10000.0	LB/DAY	1	1	3
3 CL2 FEED FROM RAIL CAR	2000.0	TO	10000.0	LB/DAY	1	1	3
4 CHLORINE DIOXIDE GENERATING,FEED	10.0	TO	3500.0	LB/DAY	2	1	4
5 OZONE GENERATION SYSTEMS	10.0	TO	3500.0	LB/DAY	0	1	2
6 OZONE CONTACT CHAMBER	460.0	TO	92000.0	CU FT	0	1	2
7 ON-SITE HYPOCHLORITE GENERATION	10.0	TO	10000.0	LB/DAY	1	1	3
8 ALUM FEED-LIQUID STOCK	5.4	TO	5400.0	LB/HR	1	1	3
9 ALUM FEED-DRY STOCK	10.0	TO	5000.0	LB/HR	1	1	3
10 POLYMER FEED SYSTEMS	1.0	TO	200.0	LB/DAY	1	10	3
11 LIME FEED-NO RECALCINATION	10.0	TO	1000.0	LB/HR	1	1	3
12 LIME FEED-WITH RECALCINATION	1000.0	TO	10000.0	LB/HR	1	8	4
13 POTASSIUM PERMANGANATE FEED	1.0	TO	500.0	LB/DAY	1	1	3
14 SULFURIC ACID FEED SYSTEMS	10.0	TO	5000.0	GPD	1	1	3
15 SODIUM HYDROXIDE FEED SYSTEMS	10.0	TO	10000.0	LB/DAY	1	1	3
16 FERROUS SULFATE FEED SYSTEMS	10.7	TO	5350.0	LB/HR	1	1	3
17 FERRIC SULFATE FEED SYSTEMS	13.3	TO	6600.0	LB/HR	1	1	3
18 ANHYDROUS AMMONIA FEED FACILITY	250.0	TO	5000.0	LB/DAY	1	1	3
19 AQUA AMMONIA FEED FACILITY	250.0	TO	5000.0	LB/DAY	1	1	3
20 POWDERED ACTIVATED CARBON FEED	3.5	TO	7000.0	LB/HR	1	1	3
21 RAPID MIX, G=300	100.0	TO	20000.0	CU FT	0	1	2
22 RAPID MIX, G=600	100.0	TO	20000.0	CU FT	0	1	2
23 RAPID MIX, G=900	100.0	TO	20000.0	CU FT	0	1	2
24 FLOCCULATION-HORIZ PADDLE, G=20	1800.0	TO	1000000.0	CU FT	0	1	2
25 FLOCCULATION-HORIZ PADDLE, G=50	1800.0	TO	1000000.0	CU FT	0	1	2
26 FLOCCULATION-HORIZ PADDLE, G=80	1800.0	TO	500000.0	CU FT	0	1	2
27 FLOCCULATION-VERT TURBINE, G=20	1800.0	TO	25000.0	CU FT	0	1	2
28 FLOCCULATION-VERT TURBINE, G=50	1800.0	TO	25000.0	CU FT	0	1	2

Table 4 (Continued)

TREATMENT PROCESS - LARGE SYSTEMS	PARAMETER RANGE			NUMBER OF CHEMICALS	PROCESS TYPE	NO. DATA CARDS	
29 FLOCCULATION-VERT TURBINE, G=80	1800.0	TO	25000.0	CU FT	0	1	2
30 CIRCULAR CLARIFIER-LIME SLUDGE	707.0	TO	31400.0	SQ FT	0	3	3
31 CIRC CLARIFIER-FECL3 & ALUM SLDG	707.0	TO	31400.0	SQ FT	0	3	3
32 RECTANGULAR CLARIFIER-LIME SLDG	240.0	TO	4800.0	SQ FT	0	3	3
33 RECT CLARIFIER-FECL3 & ALUM SLG	240.0	TO	4800.0	SQ FT	0	3	3
34 UPFLOW SOLIDS CONTACT CLAR,G=70	255.0	TO	14500.0	SQ FT	0	3	3
35 UPFLOW SOLIDS CONTACT CLAR,G=110	255.0	TO	14500.0	SQ FT	0	3	3
36 UPFLOW SOLIDS CONTACT CLAR,G=150	255.0	TO	14500.0	SQ FT	0	3	3
37 TUBE SETTLING MODULES	280.0	TO	56000.0	SQ FT	0	1	2
38 GRAVITY FILTRATION STRUCTURE	140.0	TO	28000.0	SQ FT	0	1	2
39 FILTRATION MEDIA-RAFIID SAND	370.0	TO	74800.0	SQ FT	0	1	2
40 FILTRATION MEDIA-DUAL MEDIA	140.0	TO	29900.0	SQ FT	0	1	2
41 FILTRATION MEDIA-MIXED MEDIA	140.0	TO	29900.0	SQ FT	0	1	2
42 BACKWASH PUMPING FACILITIES O&M:	1260.0	TO	23000.0	GPM	0	1	2
	1537.2	TO	28060.0	SQ FT			
43 HYDRAULIC SURFACE WASH SYSTEMS	140.0	TO	28000.0	SQ FT	0	1	2
44 AIR-WATER BACKWASH FACILITIES	140.0	TO	28000.0	SQ FT	0	1	2
45 WASH WATER SURGE BASINS	10000.0	TO	500000.0	GAL	0	1	2
46 FILTER MOD-RAP SAND TO HIGH RATE	140.0	TO	28000.0	SQ FT	0	1	2
47 CONTINUOUS AUTO. BACKWASH FILTER	360.0	TO	70400.0	SQ FT	0	1	2
48 RECARBONATION BASIN	770.0	TO	35200.0	CU FT	0	3	3
49 RECARBONATION-LIQUID CO ₂ FEED	380.0	TO	15000.0	LB/DAY	1	1	3
50 RECARB-CO ₂ FROM SUBMERGED BURNER	500.0	TO	10000.0	LB/DAY	0	3	3
51 RECARBONATION-CO ₂ FROM STACK GAS	2500.0	TO	50000.0	LB/DAY	0	1	2
52 MULTIPLE HEARTH RECALCINATION	179.0	TO	2930.0	SQ FT	0	3	3
53 CONTACT BASIN-DIRECT FILTRATION	2640.0	TO	52800.0	CU FT	0	3	3
54 PRESSURE DIATOMITE FILTERS	1.0	TO	200.0	MGD	3	2	5
55 VACUUM DIATOMITE FILTERS	1.0	TO	200.0	MGD	3	2	5

Table 4 (Continued)

TREATMENT PROCESS - LARGE SYSTEMS	PARAMETER RANGE			NUMBER OF CHEMICALS	PROCESS TYPE	NO. DATA CARDS	
56 PRESSURE FILTRATION PLANTS	140.0	TO	28000.0	SQ FT	0	1	2
57 IN-PLANT PUMPING	1.0	TO	200.0	MGD	0	5	3
58 WASH WATER STORAGE TANKS	21000.0	TO	900000.0	GAL	0	1	2
59 REVERSE OSMOSIS	1.0.	TO	200.0	MGD	3	2	5
60 PRESSURE ION EXCHANGE-SOFTENING	1.1	TO	123.0	MGD	1	1	3
61 GRAVITY ION EXCHANGE-SOFTENING	1.5	TO	150.0	MGD	1	1	3
62 PRESSURE ION EXCHANG-N03 REMOVAL	1.1	TO	12.3	MGD	1	1	3
63 ACTIV. ALUMINA-FLUORIDE REMOVAL	0.7	TO	135.0	MGD	2	2	4
64 GRAVITY GAC CONTACTORS-CONCRETE O&M:	350.0	TO	10600.0	CU FT	0	4	3
	140.0	TO	28000.0	SQ FT			
65 GRAVITY GAC CONTACTORS-STEEL O&M:	6280.0	TO	14100.0	CU FT	0	4	3
	31400.0	TO	628000.0	CU FT			
66 PRESSURE CARBON CONTACTORS O&M:	390.0	TO	2260.0	CU FT	0	4	3
	157.0	TO	6790.0	SQ FT			
67 CONVERT FILTER TO GAC CONTACTOR	370.0	TO	70000.0	SQ FT	0	1	2
68 GRANULAR ACT CARBON-CONSTR COST	10000.0	TO	10000000.0	LB	0	1	2
69 MAKEUP CARBON COST-O&M ONLY	10000.0	TO	10000000.0	LB/YR	0	1	2
70 CAPPING SAND FILTER W/ANTHRACITE	350.0	TO	70000.0	SQ FT	0	1	2
71 REGIONAL GAC REGEN-TRANS & STOR O&M:	1000.0	TO	20000.0	CU FT	0	6	3
	30000.0	TO	3000000.0	LB/YR			
72 REGIONAL MULTI HEARTH GAC REGEN	27.0	TO	1510.0	SQ FT	0	12	4
73 MULTIPLE HEARTH GAC REGENERATION	27.0	TO	1510.0	SQ FT	0	3	3
74 INFRARED CARBON REGEN FURNACE	2400.0	TO	60000.0	LB/DAY	0	1	2
75 FLUIDIZED BED GAC REGENERATION	6000.0	TO	24000.0	LB/DAY	0	3	3
76 POWDERED CARB REGEN-FLUIDIZED BD	209.0	TO	33400.0	LB/DAY	0	1	2
77 POWDERED CARB REGEN-ATOMIZED SUS	1000.0	TO	10000.0	LB/DAY	0	1	2
78 CHEM SLUDGE PUMPING-UNTHICKENED	20.0	TO	10000.0	GPM	0	1	2
79 CHEM SLUDGE PUMPING-THICKENED	5.0	TO	1250.0	GPM	0	1	2
80 GRAVITY SLUDGE THICKENER-LIME	314.0	TO	17800.0	SQ FT	0	3	3
81 GRAV SLDG THICKENER-ALUM & FECL3	314.0	TO	17800.0	SQ FT	0	3	3

Table 4 (Continued)

TREATMENT PROCESS - LARGE SYSTEMS	PARAMETER RANGE			NUMBER OF CHEMICALS	PROCESS TYPE	NO. DATA CARDS	
82 VACUUM FILTERS	9.4	TO	1320.0	SQ FT	0	1	2
83 BELT FILTER PRESS	15.0	TO	450.0	GPM	0	1	2
84 FILTER PRESS	4.3	TO	896.0	CU FT	0	1	2
85 DECANTER CENTRIFUGES	10.0	TO	500.0	GPM	0	3	3
86 BASKET CENTRIFUGES	3600.0	TO	720000.0	GPD	0	1	2
87 SAND DRYING BEDS	5000.0	TO	400000.0	SQ FT	0	1	2
88 SLUDGE DEWATERING LAGOONS O&M:	40000.0 25000.0	TO	8000000.0 5000000.0	CU FT CF/YR	0	1	2
89 SLUDGE DISPOSAL-SANITARY SEWER	20.0	TO	10000.0	GPM	0	11	3
90 LIQUID SLUDGE HAULING	1.3	TO	100.0	MG/YR	0	7	3
91 DEWATERED SLUDGE HAULING	1000.0	TO	300000.0	CY/YR	0	7	3
92 RAW WATER PUMPING FACILITY	1.0	TO	200.0	MGD	0	5	3
93 FINISHED WATER PUMPING FACILITY	1.5	TO	300.0	MGD	0	5	3
94 CLEARWELL STORAGE-BELOW GROUND	10000.0	TO	7500000.0	GAL	0	1	2
95 CLEARWELL STORAGE-GROUND LEVEL	8500.0	TO	9400000.0	GAL	0	1	2
96 DIFFUSED AERATION BASIN	1900.0	TO	380000.0	CU FT	0	1	2
97 AERATION-AERATION TOWERS	680.0	TO	256000.0	CU FT	0	1	2
98 ADMIN,LAB & MAINTENANCE BUILDING	1.0	TO	200.0	MGD	0	1	2
TREATMENT PROCESS - SMALL SYSTEMS							
99 PACKAGE COMPLETE TREATMENT PLANT	4.0	TO	1400.0	GPM	4	9	7
100 PACKAGE GRAVITY FILTER PLANTS	80.0	TO	1400.0	GPM	4	9	7
101 PACKAGE PRESSURE FILTRATION PLNT	0.7	TO	350.0	GPM	4	9	7
102 FILTER MEDIA-RAPID SAND	4.0	TO	280.0	SQ FT	0	1	2
103 FILTER MEDIA-DUAL MEDIA	4.0	TO	280.0	SQ FT	0	1	2
104 FILTER MEDIA-MIXED MEDIA	4.0	TO	280.0	SQ FT	0	1	2
105 FILTER MEDIA-MIXED,INST W/MF SUP	4.0	TO	280.0	SQ FT	0	1	2
106 PACKAGE PRESS DIATOMITE FILTERS	28000.0	TO	1000000.0	GPD	4	2	6

Table 4 (Continued)

TREATMENT PROCESS - SMALL SYSTEMS	PARAMETER RANGE				NUMBER OF CHEMICALS	PROCESS TYPE	NO. DATA CARDS
107 PACKAGE VACUUM DIATOMITE FILTERS	30.0	TO	720.0	GPM	4	2	6
108 PACKAGE ULTRAFILTRATION PLANTS	2500.0	TO	1000000.0	GPD	3	2	5
109 PACKAGE GRAN ACT CARBON COLUMNS	2500.0	TO	500000.0	GPD	0	1	2
110 POTASSIUM PERMANGANATE FEED SYST	0.1	TO	10.0	LB/DAY	1	1	3
111 POLYMER FEED SYSTEMS	0.1	TO	10.0	LB/DAY	1	10	3
112 POWDERED ACT CARBON FEED SYSTEMS	1.0	TO	10.0	LB/HR	1	1	3
113 DIRECT FEED GAS CHLORINATION	0.1	TO	100.0	LB/DAY	1	1	3
114 SODIUM HYPOCHLORITE SOLUTN FEED	0.1	TO	100.0	LB/DAY	1	1	3
115 OZONE GENERATING AND FEED	0.5	TO	10.0	LB/DAY	0	1	2
116 OZONE CONTACT CHAMBER	850.0	TO	13500.0	GAL	0	1	2
117 CHLORINE DIOXIDE GENERATING/FEED	0.1	TO	50.0	LB/DAY	2	1	4
118 ULTRAVIOLET LIGHT DISINFECTION	10.0	TO	780.0	GPM	0	1	2
119 REVERSE OSMOSIS	2500.0	TO	1000000.0	GPD	3	2	5
120 PRESSURE ION EXCHANGE-SOFTENING	70000.0	TO	860000.0	GPD	1	1	3
121 PRESSURE ION EXCHANG-NO ₃ REMOVAL	70000.0	TO	830000.0	GPD	1	1	3
122 ACTIVATED ALUMINA FLUORIDE REMOV	12700.0	TO	910000.0	GPD	2	2	4
123 BONE CHAR FLUORIDE REMOVAL	16300.0	TO	800000.0	GPD	2	1	4
124 PACKAGE RAW WATER PUMPING-TDH=50	20.0	TO	700.0	GPM	0	1	2
125 PACKAGE HIGH SERVICE PUMP STATN	30.0	TO	1100.0	GPM	0	1	2
126 STEEL BACKWASH/CLEARWELL TANKS	500.0	TO	30000.0	GAL	0	1	2
127 LIQUID SLUDGE HAULING	68.0	TO	41100.0	GPD	0	7	3
128 DEWATERED SLUDGE HAULING	100.0	TO	50000.0	CY/YR	0	7	3
129 SLUDGE DISPOSAL-SANITARY SEWER	50.0	TO	25000.0	GPD	0	11	3
130 SLUDGE DEWATERING LAGOONS O&M:	1500.0	TO	30000.0	CU FT	0	1	2
	750.0	TO	15000.0	CF/YR			
131 SAND DRYING BEDS	200.0	TO	800.0	SQ FT	0	1	2

Table 5
Processes that Use Chemicals and Chemicals Used

TREATMENT PROCESS - LARGE SYSTEMS	CHEMICALS USED
1 CL2 FEED-CYLINDER STORAGE	CHLORINE
2 CL2 FEED-ON SITE STORAGE TANK	CHLORINE
3 CL2 FEED FROM RAIL CAR	CHLORINE
4 CHLORINE DIOXIDE GENERATING,FEED	CHLORINE,SALT
7 ON-SITE HYPOCHLORITE GENERATION	SALT
8 ALUM FEED-LIQUID STOCK	ALUM-LIQUID STOCK
9 ALUM FEED-DRY STOCK	ALUM-DRY STOCK
10 POLYMER FEED SYSTEMS	POLYMER
11 LIME FEED-NO RECALCINATION	LIME
12 LIME FEED-WITH RECALCINATION	LIME
13 POTASSIUM PERMANGANATE FEED	POTASSIUM PERMANGANATE
14 SULFURIC ACID FEED SYSTEMS	SULFURIC ACID
15 SODIUM HYDROXIDE FEED SYSTEMS	SODIUM HYDROXIDE
16 FERROUS SULFATE FEED SYSTEMS	FERROUS SULFATE
17 FERRIC SULFATE FEED SYSTEMS	FERRIC SULFATE
18 ANHYDROUS AMMONIA FEED FACILITY	ANHYDROUS AMMONIA
19 AQUA AMMONIA FEED FACILITY	AQUACEOUS AMMONIA
20 POWDERED ACTIVATED CARBON FEED	POWDERED ACTIVATED CARBON
49 RECARBONATION-LIQUID CO2 FEED	LIQUID CARBON DIOXIDE
54 PRESSURE DIATOMITE FILTERS	POLYMER, ALUM, DIATOMACEOUS EARTH
55 VACUUM DIATOMITE FILTERS	POLYMER, ALUM, DIATOMACEOUS EARTH
59 REVERSE OSMOSIS	SULFURIC ACID, HEXAMETAPHOSPHATE, CHLORINE
60 PRESSURE ION EXCHANGE-SOFTENING	SALT
61 GRAVITY ION EXCHANGE-SOFTENING	SALT
62 PRESSURE ION EXCHANG-N03 REMOVAL	SALT
63 ACTIV. ALUMINA-FLUORIDE REMOVAL	SODIUM HYDROXIDE, SULFURIC ACID
TREATMENT PROCESS - SMALL SYSTEMS	
99 PACKAGE COMPLETE TREATMENT PLANT	ALUM, POLYMER, SODA ASH, CHLORINE OR HYPOCHLORITE

Table 5 (Continued)

TREATMENT PROCESS - SMALL SYSTEMS	CHEMICALS USED
100 PACKAGE GRAVITY FILTER PLANTS	ALUM, POLYMER, SODA ASH, CHLORINE OR HYPOCHLORITE
101 PACKAGE PRESSURE FILTRATION PLNT	ALUM, POLYMER, SODA ASH, CHLORINE OR HYPOCHLORITE
106 PACKAGE PRESS DIATOMITE FILTERS	ALUM, POLYMER, CHLORINE, DIATOMACEOUS EARTH
107 PACKAGE VACUUM DIATOMITE FILTERS	ALUM, POLYMER, CHLORINE, DIATOMACEOUS EARTH
108 PACKAGE ULTRAFILTRATION PLANTS	SULFURIC ACID, HEXAMETAPHOSPHATE, CHLORINE
110 POTASSIUM PERMANGANATE FEED SYST	POTASSIUM PERMANGANATE
111 POLYMER FEED SYSTEMS	POLYMER
112 POWDERED ACT CARBON FEED SYSTEMS	POWDERED ACTIVATED CARBON
113 DIRECT FEED GAS CHLORINATION	GASEOUS CHLORINE
114 SODIUM HYPOCHLORITE SOLUTN FEED	SODIUM HYPOCHLORITE
117 CHLORINE DIOXIDE GENERATING/FEED	CHLORINE, SALT
119 REVERSE OSMOSIS	SULFURIC ACID, HEXAMETAPHOSPHATE, CHLORINE
120 PRESSURE ION EXCHANGE-SOFTENING	SALT
121 PRESSURE ION EXCHANG-N03 REMOVAL	SALT
122 ACTIVATED ALUMINA FLUORIDE REMOV	SODIUM HYDROXIDE, SULFURIC ACID
123 BONE CHAR FLUORIDE REMOVAL	SODIUM HYDROXIDE, CARBONIC ACID

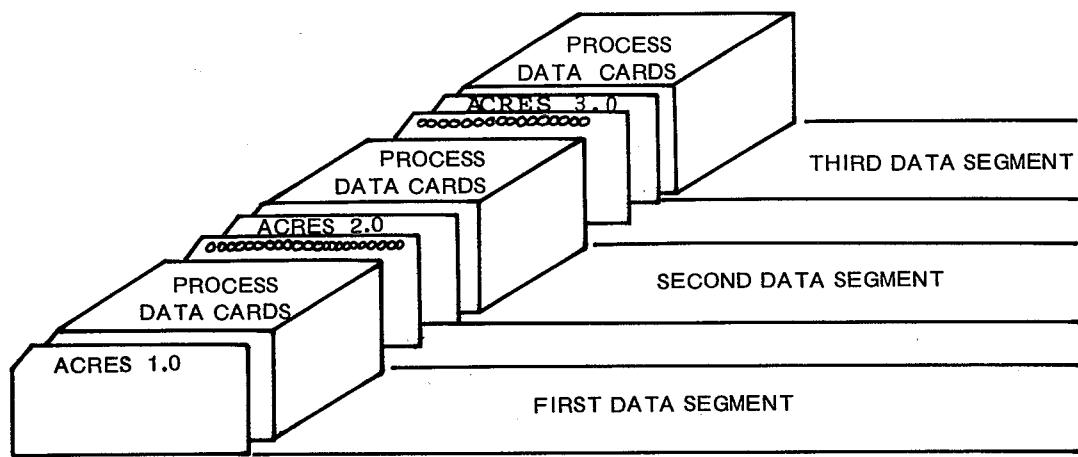


Figure 1. PROCES.DAT data segments.

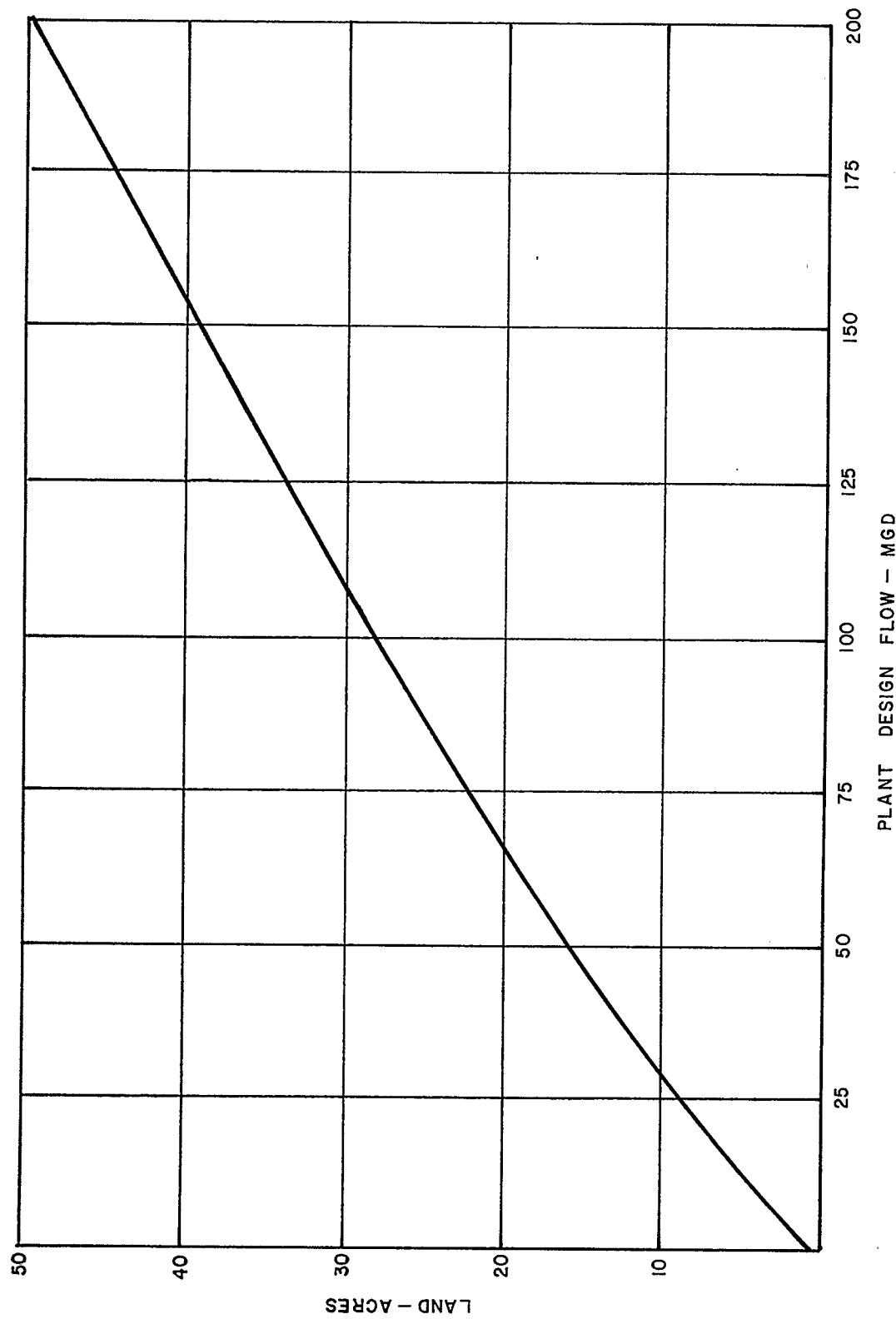


Figure 2. Land Requirements for Conventional Plants
(add area for sand drying beds or lagoons).

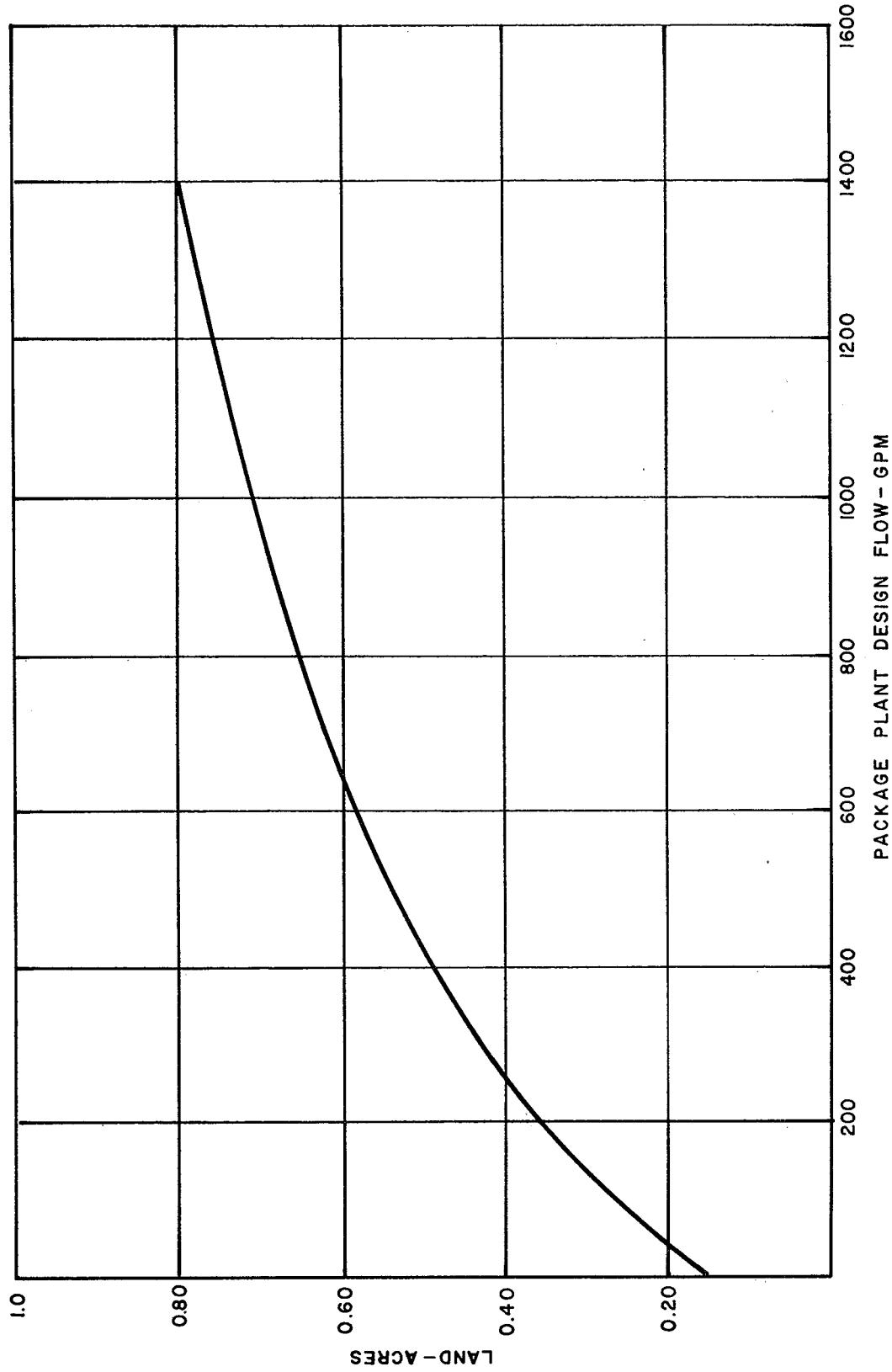


Figure 3. Land Requirements for Package Complete Treatment Plants.

THE ZERO CARD

Segments of data in the PROCES.DAT file must be separated by a card containing a string of at least 15 zeros. (In some systems, a blank card may suffice).

If cost data are desired for only one plant or segment of data, no ZERO card should be included. Inclusion of cost data for two or more plants requires that the PROCES.DAT file be arranged as shown in Figure 1, with ZERO cards between each segment.

The last card in the PROCES.DAT file is the last card of the last segment of data. A Zero card must not be placed at the end of the file. A ZERO card is only placed between segments.

PROCESS TYPES AND DATA INPUT

The various process types require two to seven cards for data input. The First two cards of data for all process types are the same. Data card format and content are explained in the following pages.

Type 1 Process Data Input

Card 1--

The first card of data contains the following information starting in column 1: The card number (the integer 1) followed by a comma in column 2, the process number (integer) from Table 3 followed immediately by a comma, and finally, the process name.

Examples:

Card 1: 1,9,ALUM FEED - DRY STOCK
Card 1: 1,21,RAPID MIX, G=300
Card 1: 1,131,SAND DRYING BEDS

The commas are necessary to separate numbers and must not be omitted. The process name is optional, but, it is a useful identifier for the user when reviewing the PROCES.DAT file later. The comma preceding the process name is not optional

Card 2--

The second card of data contains the following information starting in column 1: The card number (the integer 2) followed by a comma in column 2, the plant design flow in mgd (floating point) followed by a comma, the plant actual flow in mgd (floating point) followed by a comma, the process design parameter (floating point) followed by a comma, and the process operating parameter (floating point)

Examples: Using the same three examples as used above for Card 1, assume the following:

Example 1: Plant Design Flow = 10.0 mgd
Plant Operating Flow = 7.0 mgd
Alum Design Feed = 245 lb/hr
Alum Operating Feed = 170 lb/hr
Card 2: 2,10.0,7.0,245.0,170.0

Example 2: Plant Design Flow = 5.0 mgd
Plant Operating Flow = 4.0 mgd
Design Rapid Mix Volume = 464 cu ft
Operating Rapid Mix Volume = 464 cu ft
Card 2: 2,5.0,4.0,464.0,464.0

Example 3: Plant Design Flow = 0.5 mgd
Plant Actual Flow = 0.25 mgd
Design Sand Drying Bed Area = 500.0 sq ft
Operating Sand Drying Bed Area = 250.0 sq ft
Card 2: 2,0.5,0.25,500.0,250.0

The process design and operating parameters have the units specified in Tables 4 and 6. The process design parameter is used to calculate construction costs, and the operating parameter is used to determine operation and maintenance costs. In some cases, these parameters have different units and/or ranges. In Table 4, for example, process 42 (BACKWASH PUMPING FACILITIES) has the unit gpm for the design parameter and sq ft for the operating parameter. Plant flows are always in mgd. All values are floating point (except the card number) and are separated by a comma. Notice that for some processes such as chemical feed and pumping, the numerical values of the design and operating parameters may be different, since the design parameter indicates capacity, and these processes generally do not operate at capacity. For other processes, such as basins, the design and operating parameters are identical. Operation and maintenance costs for any process operating at less than 100 percent time can be determined by inputting a proportionately lower value for the operating parameter. For example, operation and maintenance costs for a 500 sq ft furnace operating 70 percent of the time are determined by inputting a value of 350 for the operating parameter.

Cards 3 and 4--

The number of cards for a type 1 process is equal to 2 plus the number of chemicals. For example, process number 9, ALUM FEED - DRY STOCK, requires $2 + 1 = 3$ cards. Process 21 (RAPID MIX, G=300) requires $2 + 0 = 2$ cards.

If a third or fourth card of data is required, it contains the following information: The number of the card (the integer 3 or 4) followed by a comma, the cost of the chemical(s) used in the process in dollars/ton (floating point) followed by a comma, and the name of the chemical used in the process (up to 24 characters). For most processes, the chemical(s) used will be

Table 6
Process Parameter Units

TREATMENT PROCESS - LARGE SYSTEMS	UNITS
1 CL2 FEED-CYLINDER STORAGE	LB/DAY OF CHLORINE
2 CL2 FEED-ON SITE STORAGE TANK	LB/DAY OF CHLORINE
3 CL2 FEED FROM RAIL CAR	LB/DAY OF CHLORINE
4 CHLORINE DIOXIDE GENERATING,FEED	LB/DAY OF CHLORINE DIOXIDE
5 OZONE GENERATION SYSTEMS	LB/DAY OF OZONE
6 OZONE CONTACT CHAMBER	CU FT OF TOTAL CHAMBER VOLUME
7 ON-SITE HYPOCHLORITE GENERATION	LB/DAY OF EQUIVALENT CHLORINE
8 ALUM FEED-LIQUID STOCK	LB/HR OF ALUM
9 ALUM FEED-DRY STOCK	LB/HR OF ALUM
10 POLYMER FEED SYSTEMS	LB/DAY OF POLYMER
11 LIME FEED-NO RECALCINATION	LB/HR OF LIME
12 LIME FEED-WITH RECALCINATION	LB/HR OF LIME
13 POTASSIUM PERMANGANATE FEED	LB/DAY OF PERMANGANATE
14 SULFURIC ACID FEED SYSTEMS	GPD OF SULFURIC ACID
15 SODIUM HYDROXIDE FEED SYSTEMS	LB/DAY OF SODIUM HYDROXIDE
16 FERROUS SULFATE FEED SYSTEMS	LB/HR OF FERROUS SULFATE
17 FERRIC SULFATE FEED SYSTEMS	LB/HR OF FERRIC SULFATE
18 ANHYDROUS AMMONIA FEED FACILITY	LB/DAY OF AMMONIA
19 AQUA AMMONIA FEED FACILITY	LB/DAY OF AMMONIA
20 POWDERED ACTIVATED CARBON FEED	LB/HR OF POWDERED CARBON
21 RAPID MIX, G=300	CU FT OF TOTAL BASIN VOLUME
22 RAPID MIX, G=600	CU FT OF TOTAL BASIN VOLUME
23 RAPID MIX, G=900	CU FT OF TOTAL BASIN VOLUME
24 FLOCCULATION-HORIZ PADDLE, G=20	CU FT OF TOTAL BASIN VOLUME
25 FLOCCULATION-HORIZ PADDLE, G=50	CU FT OF TOTAL BASIN VOLUME
26 FLOCCULATION-HORIZ PADDLE, G=80	CU FT OF TOTAL BASIN VOLUME
27 FLOCCULATION-VERT TURBINE, G=20	CU FT OF TOTAL BASIN VOLUME
28 FLOCCULATION-VERT TURBINE, G=50	CU FT OF TOTAL BASIN VOLUME

Table 6 (Continued)

TREATMENT PROCESS - LARGE SYSTEMS	UNITS
29 FLOCCULATION-VERT TURBINE, G=80	CU FT OF TOTAL BASIN VOLUME
30 CIRCULAR CLARIFIER-LIME SLUDGE	SQ FT OF SINGLE CLARIFIER AREA
31 CIRC CLARIFIER-FECL3 & ALUM SLDG	SQ FT OF SINGLE CLARIFIER AREA
32 RECTANGULAR CLARIFIER-LIME SLDG	SQ FT OF SINGLE CLARIFIER AREA
33 RECT CLARIFIER-FECL3 & ALUM SLDG	SQ FT OF SINGLE CLARIFIER AREA
34 UPFLOW SOLIDS CONTACT CLAR,G=70	SQ FT OF SINGLE CLARIFIER AREA
35 UPFLOW SOLIDS CONTACT CLAR,G=110	SQ FT OF SINGLE CLARIFIER AREA
36 UPFLOW SOLIDS CONTACT CLAR,G=150	SQ FT OF SINGLE CLARIFIER AREA
37 TUBE SETTLING MODULES	SQ FT OF TOTAL TUBE MODULE AREA
38 GRAVITY FILTRATION STRUCTURE	SQ FT OF TOTAL FILTER AREA
39 FILTRATION MEDIA-RAPID SAND	SQ FT OF TOTAL FILTER AREA
40 FILTRATION MEDIA-DUAL MEDIA	SQ FT OF TOTAL FILTER AREA
41 FILTRATION MEDIA-MIXED MEDIA	SQ FT OF TOTAL FILTER AREA
42 BACKWASH PUMPING FACILITIES O&M:	GPM OF BACKWASH PUMPING CAPACITY SQ FT OF TOTAL FILTER AREA
43 HYDRAULIC SURFACE WASH SYSTEMS	SQ FT OF TOTAL FILTER AREA
44 AIR-WATER BACKWASH FACILITIES	SQ FT OF TOTAL FILTER AREA
45 WASH WATER SURGE BASINS	GAL OF BASIN VOLUME
46 FILTER MOD-RAP SAND TO HIGH RATE	SQ FT OF TOTAL FILTER AREA
47 CONTINUOUS AUTO. BACKWASH FILTER	SQ FT OF TOTAL FILTER AREA
48 RECARBONATION BASIN	CU FT OF SINGLE BASIN VOLUME
49 RECARBONATION-LIQUID CO ₂ FEED	LB/DAY OF LIQUID CARBON DIOXIDE
50 RECARB-CO ₂ FROM SUBMERGED BURNER	LB/DAY OF CARBON DIOXIDE FROM SINGLE BURNER SET
51 RECARBONATION-CO ₂ FROM STACK GAS	LB/DAY OF CARBON DIOXIDE
52 MULTIPLE HEARTH RECALCINATION	SQ FT OF SINGLE FURNACE EFFECTIVE HEARTH AREA
53 CONTACT BASIN-DIRECT FILTRATION	CU FT OF SINGLE BASIN AREA
54 PRESSURE DIATOMITE FILTERS	MGD OF TOTAL FILTER FLOW
55 VACUUM DIATOMITE FILTERS	MGD OF TOTAL FILTER FLOW

Table 6 (Continued)

TREATMENT PROCESS - LARGE SYSTEMS	UNITS
56 PRESSURE FILTRATION PLANTS	SQ FT OF TOTAL FILTER AREA
57 IN-PLANT PUMPING	MGD OF TOTAL PLANT FLOW
58 WASH WATER STORAGE TANKS	GAL OF TOTAL TANK VOLUME
59 REVERSE OSMOSIS	MGD OF TOTAL FLOW
60 PRESSURE ION EXCHANGE-SOFTENING	MGD OF TOTAL FLOW
61 GRAVITY ION EXCHANGE-SOFTENING	MGD OF TOTAL FLOW
62 PRESSURE ION EXCHANG-N03 REMOVAL	MGD OF TOTAL FLOW
63 ACTIV. ALUMINA-FLUORIDE REMOVAL	MGD OF TOTAL FLOW
64 GRAVITY GAC CONTACTORS-CONCRETE O&M:	CU FT OF SINGLE CONTACTOR VOLUME SQ FT OF TOTAL CONTACTOR AREA
65 GRAVITY GAC CONTACTORS-STEEL O&M:	CU FT OF SINGLE VOLUME CU FT OF TOTAL CONTACTOR VOLUME
66 PRESSURE CARBON CONTACTORS O&M:	CU FT OF SINGLE CONTACTOR VOLUME SQ FT OF TOTAL CONTACTOR AREA
67 CONVERT FILTER TO GAC CONTACTOR	SQ FT OF TOTAL FILTER AREA
68 GRANULAR ACT CARBON-CONSTR COST	LB OF TOTAL CARBON WEIGHT
69 MAKEUP CARBON COST-O&M ONLY	LB/YR OF TOTAL CARBON WEIGHT
70 CAPPING SAND FILTER W/ANTHRACITE	SQ FT OF TOTAL FILTER AREA
71 REGIONAL GAC REGEN-TRANS & STOR O&M:	CU FT OF ON-SITE CARBON STORAGE CAPACITY LB/YR OF CARBON REGENERATED
72 REGIONAL MULTI HEARTH GAC REGEN	SQ FT OF SINGLE FURNACE EFFECTIVE HEARTH AREA
73 MULTIPLE HEARTH GAC REGENERATION	SQ FT OF SINGLE FURNACE EFFECTIVE HEARTH AREA
74 INFRARED CARBON REGEN FURNACE	LB/DAY OF TOTAL CARBON WEIGHT
75 FLUIDIZED BED GAC REGENERATION	LB/DAY OF CARBON FOR SINGLE FURNACE
76 POWDERED CARB REGEN-FLUIDIZED BD	LB/DAY OF TOTAL CARBON WEIGHT
77 POWDERED CARB REGEN-ATOMIZED SUS	LB/DAY OF TOTAL CARBON WEIGHT
78 CHEM SLUDGE PUMPING-UNTHICKENED	GPM OF SLUDGE PUMPING
79 CHEM SLUDGE PUMPING-THICKENED	GPM OF SLUDGE PUMPING
80 GRAVITY SLUDGE THICKENER-LIME	SQ FT OF SINGLE BASIN AREA
81 GRAV SLDG THICKENER-ALUM & FECL3	SQ FT OF SINGLE BASIN AREA

Table 6 (Continued)

TREATMENT PROCESS - LARGE SYSTEMS	UNITS
82 VACUUM FILTERS	SQ FT OF TOTAL FILTER AREA
83 BELT FILTER PRESS	GPM OF TOTAL SLUDGE PUMPING
84 FILTER PRESS	CU FT OF PRESS SLUDGE CAPACITY
85 DECANTER CENTRIFUGES	GPM OF SLUDGE PUMPING
86 BASKET CENTRIFUGES	GPD OF SLUDGE PUMPING
87 SAND DRYING BEDS	SQ FT OF TOTAL BED AREA
88 SLUDGE DEWATERING LAGOONS O&M:	CU FT OF TOTAL LAGOON VOLUME CF/YR OF SLUDGE REMOVED
89 SLUDGE DISPOSAL-SANITARY SEWER	GPM OF SLUDGE
90 LIQUID SLUDGE HAULING	MG/YR OF SLUDGE
91 DEWATERED SLUDGE HAULING	CY/YR OF SLUDGE
92 RAW WATER PUMPING FACILITY	MGD OF TOTAL FLOW
93 FINISHED WATER PUMPING FACILITY	MGD OF TOTAL FLOW
94 CLEARWELL STORAGE-BELOW GROUND	GAL OF CLEARWELL VOLUME
95 CLEARWELL STORAGE-GROUND LEVEL	GAL OF CLEARWELL VOLUME
96 DIFFUSED AERATION BASIN	CU FT OF BASIN VOLUME
97 AERATION-AERATION TOWERS	CU FT OF TOWER VOLUME
98 ADMIN,LAB & MAINTENANCE BUILDING	MGD OF PLANT FLOW
TREATMENT PROCESS - SMALL SYSTEMS	
99 PACKAGE COMPLETE TREATMENT PLANT	GPM OF TOTAL FLOW
100 PACKAGE GRAVITY FILTER PLANTS	GPM OF TOTAL FLOW
101 PACKAGE PRESSURE FILTRATION PLNT	GPM OF TOTAL FLOW
102 FILTER MEDIA-RAPID SAND	SQ FT OF TOTAL FILTER AREA
103 FILTER MEDIA-DUAL MEDIA	SQ FT OF TOTAL FILTER AREA
104 FILTER MEDIA-MIXED MEDIA	SQ FT OF TOTAL FILTER AREA
105 FILTER MEDIA-MIXED,INST W/MF SUP	SQ FT OF TOTAL FILTER AREA
106 PACKAGE PRESS DIATOMITE FILTERS	GPD OF TOTAL FILTER FLOW

Table 6 (Continued)

TREATMENT PROCESS - SMALL SYSTEMS		UNITS
107 PACKAGE VACUUM DIATOMITE FILTERS	GPM	OF TOTAL FILTER FLOW
108 PACKAGE ULTRAFILTRATION PLANTS	GPD	OF TOTAL FLOW
109 PACKAGE GRAN ACT CARBON COLUMNS	GPD	OF TOTAL FLOW
110 POTASSIUM PERMANGANATE FEED SYST	LB/DAY	OF PERMANGANATE
111 POLYMER FEED SYSTEMS	LB/DAY	OF POLYMER
112 POWDERED ACT CARBON FEED SYSTEMS	LB/HR	OF POWDERED CARBON
113 DIRECT FEED GAS CHLORINATION	LB/DAY	OF CHLORINE
114 SODIUM HYPOCHLORITE SOLUTN FEED	LB/DAY	OF EQUIVALENT CHLORINE
115 OZONE GENERATING AND FEED	LB/DAY	OF OZONE
116 OZONE CONTACT CHAMBER	GAL	OF TOTAL CHAMBER VOLUME
117 CHLORINE DIOXIDE GENERATING/FEED	LB/DAY	OF CHLORINE DIOXIDE
118 ULTRAVIOLET LIGHT DISINFECTION	GPM	OF TOTAL FLOW
119 REVERSE OSMOSIS	GPD	OF FLOW
120 PRESSURE ION EXCHANGE-SOFTENING	GPD	OF FLOW
121 PRESSURE ION EXCHANG-N03 REMOVAL	GPD	OF FLOW
122 ACTIVATED ALUMINA FLUORIDE REMOV	GPD	OF FLOW
123 BONE CHAR FLUORIDE REMOVAL	GPD	OF FLOW
124 PACKAGE RAW WATER PUMPING-TDH=50	GPM	OF FLOW
125 PACKAGE HIGH SERVICE PUMP STATN	GPM	OF FLOW
126 STEEL BACKWASH/CLEARWELL TANKS	GAL	OF TOTAL TANK VOLUME
127 LIQUID SLUDGE HAULING	GPD	OF SLUDGE
128 DEWATERED SLUDGE HAULING	CY/YR	OF SLUDGE
129 SLUDGE DISPOSAL-SANITARY SEWER	GPD	OF SLUDGE
130 SLUDGE DEWATERING LAGOONS O&M:	CU FT CF/YR	OF TOTAL LAGOON VOLUME OF SLUDGE REMOVED
131 SAND DRYING BEDS	SQ FT	OF TOTAL BED AREA

obvious. For example, process 9 (ALUM FEED - DRY STOCK) uses alum. For convenience, however, the processes that use chemicals and the names of the chemicals are shown in Table 5.

Examples: Alum = \$70.00/ton

Card 3: 3,70.00,ALUM

Since the 24 characters immediately following the second comma are copied on the printout, other useful information may be included. For example, we could have written:

Card 3: 3,70.00,ALUM (DOSE = 70 MG/L)

Any characters following the 24th character will be ignored.

Completed Examples--

The following four examples show all cards necessary for data input of the processes shown. All data begin in column one.

Card 1: 1,9,ALUM FEED - DRY STOCK

Card 2: 2,10.0,7.0,245.0,170.0

Card 3: 3,70.0,ALUM (DOSE = 70 MG/L)

Card 1: 1,21,RAPID MIX, G=300

Card 2: 2,5.0,4.0,464.0,464.0

Card 1: 1,131,SAND DRYING BEDS

Card 2: 2,0.5,0.25,500.0,500.0

Card 1: 1,4,CHLORINE DIOXIDE GENERATING,FEED

Card 2: 2,2.0,1.75,16.7,14.5

Card 3: 3,300.0,CHLORINE

Card 4: 4,225.0,SODIUM CHLORITE

The first three examples were explained above. The last example can be interpreted as follows:

Total number of cards necessary is 2 + number of chemicals = 2 + 2 = 4.

Card 1: Process No. 4, CHLORINE DIOXIDE GENERATING - FEED

Card 2: Design flow = 2.0 mgd, actual flow = 1.75 mgd, process design parameter = 16.7 lb/day, process operating parameter = 14.5 lb/day

Card 3: \$300.00/ton for chlorine used in this process

Card 4: \$225.00/ton for sodium chlorite used in this process

Type 2 Process Data Input

The total number of data cards required for a type 2 process is 2 + number of chemicals. The first two cards of data are identical in format

and content to a type 1 process. The remaining cards contain chemical cost and chemical feed information. For example, process 59 (REVERSE OSMOSIS) may use up to 3 chemicals: sulfuric acid, sodium hexameta phosphate, and chlorine. This process requires $2 + 3 = 5$ cards of data with the following information: The card number (integer) followed by a comma, the cost of the chemical in \$/ton (floating point) followed by a comma, the actual (not design) feed rate in lb/day for the chemical (floating point) followed by a comma, and the name of the chemical (not to exceed 24 characters). The chemicals can be input in any order. If one or more of the chemicals is not used, an input of zeros for the chemical cost and the chemical feed rate will cause no information to be printed on the output for that chemical. To illustrate, the 5 data cards for process 59 (REVERSE OSMOSIS) may be constructed as follows:

Card 1: 1,59,REVERSE OSMOSIS
Card 2: 2,2.0,1.5,2.0,1.5
Card 3: 3,650.0,250.2,SULFURIC ACID,20 MG/L
Card 4: 4,650.0,62.6,SODIUM HEXA PO3,5 MG/L
Card 5: 5,300.0,25.0,CHLORINE,2 MG/L

Card 1: 1,59,REVERSE OSMOSIS
Card 2: 2,2.0,1.5,2.0,1.5
Card 3: 3,650.0,62.5,SODIUM HEXA PO3,5 MG/L
Card 4: 4,650.0,125.1,SULFURIC ACID,10 MG/L
Card 5: 5,0.0,0.0

Card 1: 1,59,REVERSE OSMOSIS
Card 2: 2,2.0,1.5,2.0,1.5
Card 3: 3,0.0,0.0
Card 4: 4,0.0,0.0
Card 5: 5,0.0,0.0

Example 1, above, indicates the following:

Card 3: \$65.00/ton cost and 250.2 lb/day feed rate for sulfuric acid at a dose of 20 mg/l
Card 4: \$650.00/ton and 62.6 lb/day feed rate for sodium hexameta phosphate at a dose of 5 mg/l
Card 5: \$300.00/ton and 25.0 lb/day feed rate for chlorine at 2 mg/l

Example 2, above, indicates the following:

Card 3: \$650.00/ton for sodium hexameta phosphate at a 5 mg/l dose
Card 4: \$65.00/ton for sulfuric acid at a 10 mg/l dose
Card 5: No other chemicals used

Example 3, above, indicates that no chemicals were used in this process since cards 3 to 5 contained zeros for the chemicals costs and feed rates.

Type 3 Process Data Input

The total number of cards required for a type 3 process is 3 + number of chemicals. The first two lines are identical in form and content to the first two lines of process type 1. Card 3 is very specific and must contain the number of units of the process in question for which costs are desired. For example, process 31 (CIRC CLARIFIER - FECL3 & ALUM SLDG), when input to the computer, calculates costs for a single clarifier. The program then multiplies the calculated costs for a single clarifier by the number of units indicated on card 3.

To illustrate this, consider the following process data input. Total number of data cards = 3 + 0 = 3.

Card 1: 1,31,CIRC CLARIFIER - FECL3 & ALUM SLDG
Card 2: 2,1.0,0.9,1667.0,1667.0
Card 3: 3,1,UNIT

Card 3 above contains the integer 3 beginning in column 1 followed by a comma, and the number of units (integer) for which costs are desired followed by a comma and the word UNIT or UNITS. The word UNIT(S) is optional, but the comma following the number of units is not. Costs could be obtained for three 1667.0 sq ft clarifiers by either of the following methods (more about this later):

Card 1: 1,31,CIRC CLARIFIER - FECL3 & ALUM SLDG
Card 2: 2,3.0,2.7,1667.0,1667.0
Card 3: 3,3,UNIT

or,

Card 1: 1,31,CIRC CLARIFIER - FECL3 & ALUM SLDG
Card 2: 2,1.0,0.9,1667.0,1667.0
Card 3: 3,1,UNIT
Card 1: 1,31,CIRC CLARIFIER - FECL3 & ALUM SLDG
Card 2: 2,1.0,0.9,1667.0,1667.0
Card 3: 3,1,UNIT
Card 1: 1,31,CIRC CLARIFIER - FECL3 & ALUM SLDG
Card 2: 2,1.0,0.9,1667.0,1667.0
Card 3: 3,1,UNIT

The above example shows that the design and operating flows in card 2 of each process represent the total flow for that process only. The first example, gives a total of 2.7 mgd (0.9 mgd/clarifier x 3 clarifiers), and the second example yields a flow of 0.9 mgd for each clarifier.

If the number of chemicals for any type 3 process is greater than 1, the additional cards will contain chemical cost information identical in format and content to the third card of process type 1.

Type 4 Process Data Input

The number of data cards required for type 4 processes (GAC Contactors) is $3 + \text{number of chemicals}$ or $3 + 0 = 3$ cards of data. The first two cards of data are identical in format and content to type 1. The third data card is identical in form and content to the third data card of type 3 processes. Note, however, that the design process variable has the units of cu ft per single contactor volume, and the operating process variable has the units of total volume in cu ft or total area in sq ft (see Table 6). For example, consider the following data cards for process 65 (GRAVITY GAC CONTACTORS - STEEL): The design flow is 50.0 mgd, the actual flow is 30.0 mgd, the single contactor volume is 6,300 cu ft, the number of contactors is 22, and the total volume is 138,600 cu ft.

Card 1: 1,65,GRAVITY GAC CONTACTORS - STEEL
Card 2: 2,50.0,30.0,6300.0,138600.0
Card 3: 3,22,UNITS

There are only 3 type 4 processes. All are granular activated carbon treatment. The operation and maintenance cost curves for each include the costs for backwash pumping for the contactors. The cost for backwash pumping is different for each type of contactor because of the variation in the pumping head. Therefore, when computing costs for a train of processes that includes any of the activated carbon contactors (processes 64, 65 or 66) and backwash pumping for these contactors (process 42), a zero must be input for the operating parameter of the backwash pumping curve. This will avoid duplication of the operation and maintenance costs for backwash pumping.

Type 5 Process Data Input

The number of data cards for type 5 is $3 + \text{number of chemicals}$ or $3 + 0 = 3$. Type 5 processes consist of the various types of pumping facilities. Cards 1 and 2 are identical in format and content to cards 1 and 2 of type 1. Card 3 contains the integer 3 followed by a comma, the total dynamic pumping head in feet (floating point) followed by a comma, and the abbreviation TDH.

For example, process 57 (IN PLANT PUMPING) for a 5.0 mgd plant with an actual flow of 3.0 mgd and a total dynamic head of 40 ft becomes:

Card 1: 1,57,IN-PLANT PUMPING
Card 2: 2,5.0,3.0,7.5,3.0
Card 3: 3,40.0,TDH

In this case, a 7.5 mgd pumping capacity has been installed as shown in Card 2. The abbreviation TDH is optional, but the comma preceding it is not.

Type 6 and 7 Process Data Input

The number of data cards required for types 6 and 7 is $3 + \text{number of chemicals}$ = $3 + 0 = 3$. The first two data cards of types 6 and 7 are

identical in format and content to type 1. The third card of data contains the number of one-way miles driven to the regeneration site or the sludge disposal site. Similar to previous processes, Card 3 contains the integer 3 followed by a comma, the number of one-way miles (floating point) followed by a comma, and the word MILES. The word MILES is optional, but the comma preceding it is not.

Examples:

Card 1: 1,71,REGIONAL GAC REGEN-TRANS & STOR
Card 2: 2,1.0,0.9,1000.0,30000.0
Card 3: 3,10.0,MILES

Card 1: 1,90,LIQUID SLUDGE HAULING
Card 2: 2,1.0,1.0,1.3,1.3
Card 3: 3,15.0,MILES

Type 8 Process Data Input

The number of data cards for type 8 is $3 + \text{number of chemicals} = 3 + 1 = 4$. The first two data cards are identical in format and content to the first two data cards of type 1. The third data card contains the integer 3 followed by a comma, the amount of makeup lime added to the recalcined lime is percent of lime feed rate (floating point) followed by a comma, and the words MAKEUP LIME %. The words MAKEUP LIME % are optional, but the preceding comma is not. The fourth card of data contains chemical cost information and is similar to the third card of type 1.

Examples for 5% and 10% makeup lime:

Card 1: 1,12,LIME FEED - WITH RECALCINATION
Card 2: 2,30.0,25.0,3500.0,2606.0
Card 3: 3,5.0,MAKEUP LIME %
Card 4: 4,40.0,LIME

Card 1: 1,12,LIME FEED - WITH RECALCINATION
Card 2: 2,30.0,25.0,3500.0,2606.0
Card 3: 3,10.0,MAKEUP LIME %
Card 4: 4,40.0,LIME

In the above examples, the cost of lime is \$40.00/ton, the plant design flow is 30.0 mgd, and the design lime rate is 3500.0 lb/hr. In the fourth data card, the word LIME is not optional. Chemical names following chemical cost information are not optional unless the amount or the cost of that chemical is zero.

Type 9 Process Data Input

The total number of data cards required for type 9 is $3 + \text{number of chemicals} = 3 + 4 = 7$. This process type includes the package treatment plants, which may use from zero to 4 chemicals, depending on the operators' requirements. The first two data cards are identical in format and content

to the first two data cards of type 1. The third data card contains the integer 3 followed by a comma, the hydraulic loading on the package plant in gpm/sf (floating point) followed by a comma, and the abbreviation gpm/sf. The abbreviation, gpm/sf is optional, but the preceding comma is not. The fourth, fifth, sixth and seventh data cards contain chemical cost and chemical feed information with format and content identical to chemical information cards for type 2 processes. That is, they contain the card number (integer) followed by a comma, the cost of the chemical used is \$/ton (floating point) followed by a comma, the chemical feed rate is lb/day (floating point) followed by a comma, and the name of the chemical (up to 24 characters long). If a chemical name is input exceeding 24 characters, the 25th and succeeding characters will be ignored.

Example:

Card 1: 1,99,PACKAGE COMPLETE TREATMENT PLANT
Card 2: 2,0.288,0.252,200.0,175.0
Card 3: 3,2.0,GPM/SF
Card 4: 4,70.0,147.0,ALUM,70 MG/L
Card 5: 5,4000.0,2.0,POLYMER,1 MG/L(\$2/LB)
Card 6: 5,0.0,0.0
Card 7: 7,0.0,0.0

Type 10 Process Data Input

The total number of cards for type 10 is 2 + number of chemicals =
 $2 + 1 = 3$.

The data card input is identical in format and content to type 1 for all cards with one exception. The chemical cost is input in \$/lb instead of \$/ton.

Example:

Card 1: 1,10,POLYMER FEED SYSTEMS
Card 2: 2,1.0,1.0,8.34,8.34
Card 3: 3,2.0, POLYMER,1 MG/1

Refer to section on type 1 process data input for a discussion of format and content of data cards.

Type 11 Process Data Input

The total number of data cards for type 11 is 3 + number of chemicals =
 $3 + 0 = 3$. The first two data cards are identical in format and content to the first two data cards of type 1. The third data card for process 11 contains the integer 3 followed by a comma, the sludge concentration in mg/l (floating point) followed by a comma, and the abbreviation mg/l. The abbreviation mg/l is optional, but the preceding comma is not.

Example:

Card 1: 1,89,SLUDGE DISPOSAL - SANITARY SEWER
Card 2: 2,1.0,1.0,20.0,20.0
Card 3: 3,10000.0,MG/L

Type 12 Process Data Input

The total number of cards for type 12 is 4 + number of chemicals = $4 + 0 = 4$. The first two data cards are identical in format and content to the first two data cards of type 1. The third data card indicates the number of units and is identical to the third data card of type 3. The fourth data card indicates percent ownership of the regional facility and contains the integer 4 followed by a comma, the percent ownership (floating point) followed by a comma, and the optional words % OWNERSHIP. The comma preceding % OWNERSHIP is not optional.

Example:

Card 1: 1,72,REGIONAL MULTI HEARTH GAC REGEN
Card 2: 2,5.0,3.5,800.0,560.0
Card 3: 3,2,UNITS
Card 4: 4,10.0% OWNERSHIP

SECTION 5

PROGRAM OUTPUT

DETAILED OR SUMMARY

Program output is controlled by both the COST.DAT file and the PROCES.DAT file. The main option available to the user is determined in line 28 of the COST.DAT file. The two options available are the DETAILED or SUMMARY printout. Sample printouts for each of the options are shown in Examples 1 through 3 in Section 6. Note that if the user chooses the DETAILED printout, he gets all the information contained in the SUMMARY plus a detailed cost breakdown for each process.

REPETITIVE OUTPUT

Program output is also controlled, in part, by the way in which the COST.DAT and PROCES.DAT files are constructed. In Section 3, COST.DAT File Construction, it was shown that two additional cards of data could be added (cards 29 and 30) to the file to cause the program to be rerun. Card 29 designates which cost factor is to be changed during the rerun, and card 30 contains the values to be used during the rerun. In other words, if cards 29 and 30 were added to the COST.DAT file with the following information,

Card 29: 8,2
Card 30: 0.02,0.04

the program would be rerun twice using the existing PROCES.DAT file and the new values, 0.02 and 0.04, of cost factor number 8, ELECTRICITY, \$/kwh. This has the same effect as running the program three times. This is, three complete program output listings will be generated: One complete output computing costs with the original cost of electricity, one complete output computing costs with electricity at \$0.02/kwh, and one complete output computing costs with electricity at \$0.04/kwh.

In Section 4, PROCES.DAT File Construction, it was shown that data were input or assembled as segments, with a segment representing costs for one treatment plant. A complete program output includes computed costs listed separately for each data segment, with a listing of the COST.DAT file following the output for the final data segment. Therefore, if the PROCES.DAT file were constructed with five data segments and the COST.DAT file contained cards of 29 and 30, as shown above, the printout generated by the program would consist of:

1st data segment cost information
2nd data segment cost information
3rd data segment cost information
4th data segment cost information
5th data segment cost information
Listing of COST.DAT values used

1st data segment cost information

.

.

5th data segment cost information

Listing of COST.DAT values used (as above except electricity = \$0.02/kwh)

1st data segment cost information

.

.

5th data segment cost information

Listing of COST.DAT values used (as above except electricity = \$0.04/kwh)

Examples of the above program outputs are shown in Section 6, Examples.

COST EXTRAPOLATION FOR OUT-OF-RANGE INPUTS

Table 4 lists the processes for which costs are available and the design and operating parameter ranges over which these costs are valid. If the user attempts to obtain costs for process parameters outside the valid range, the program will extrapolate the stored costs and notify the user of this condition on the printout. The extrapolation is accomplished by evaluating the following equation for y after first computing the constants C_1 and C_2 from stored cost data:

$$\ln y = C_1 + C_2 \ln x$$

Where x is the input process parameter (out of range) and y is the extrapolated cost at x .

When plotted on log-log paper, this results in a linear extrapolation of the cost curve. See Section 6, EXAMPLES, for a sample printout of extrapolated costs.

SECTION 6

EXAMPLES

The following examples have been constructed to demonstrate the options of input and output available. Each example is arranged with a table of the plant and process assumptions followed by copies of the actual COST.DAT and PROCES.DAT files and the program output.

EXAMPLE 1

Example 1 contains one segment of data with five treatment processes in the PROCES.DAT file. The COST.DAT file contains the DETAILED printout option and the use of the ENR Construction Cost Index. The COST.DAT and PROCES.DAT files are shown along with the printout generated by these inputs.

EXAMPLE 2

Example 2 contains two segments of data with 17 and 4 treatment processes, respectively, in the PROCES.DAT file. The COST.DAT file contains the SUMMARY printout option and does not use the ENR Construction Cost Index. The COST.DAT and PROCES.DAT files are shown along with the printouts generated by these inputs.

EXAMPLE 3

Example 3 contains two segments of data with 6 and 1 treatment processes, respectively, in the PROCES.DAT file. The COST.DAT file contains the SUMMARY printout option and does not use the ENR Construction Cost Index. The COST.DAT file also contains lines 29 and 30, which causes additional printouts varying the cost of labor to include \$7.50/hr and \$12.50/hr. The COST.DAT and PROCES.DAT files are shown along with the printouts generated by these inputs.

COST.DAT File

Example 1

COSTS PRESENTED ARE CURRENT AS OF OCTOBER 1978
CAPITAL COST FACTORS (% OF CONSTRUCTION COST):

1 ENGINEERING(%) =10.
2 SITWORK, INTERFACE PIPING(%) =5.
3 SUBSURFACE CONSIDERATIONS(%) =0.0
4 STANDBY POWER(%) =0.0
5 INTEREST RATE(%) =7.
6 NUMBER OF YEARS =20.0
7 LAND COST, \$/ACRE =2000.

UNIT COST FACTORS:

8 ELECTRICITY, \$/KWH =.03
9 LABOR, \$/HR =10.
10 DIESEL FUEL, \$/GAL =.45
11 NATURAL GAS, \$/CU FT =.0013
12 BLDNG ENERGY USE,KWH/SQ FT/YR =102.6

COST INDEXES:

13 EXCAVATION(ENR SKILLED LABOR) =247.0
14 MANUFACTURED EQUIP (BLS #114) =221.3
15 CONCRETE (BLS #132) =221.1
16 STEEL (BLS #101.3) =262.1
17 LABOR (ENR SKILLED LABOR) =247.0
18 PIPE & VALVES (BLS #114.901) =236.4
19 ELECTRICAL & INSTR (BLS #117) =167.5
20 HOUSING (ENR BUILDING COST) =254.76
21 PRODUCER PRICE INDEX =199.7
22 ENR CONSTRUCTION, '67 BASE YR =265.38
OUTPUT(6 FOR LP,5 FOR TELETYPE) =5
PRINTOUT(DETAILED OR SUMMARY) =DETAILED

PROCES.DAT File

Example 1

```
ACRES=0.25
1,124,PACKAGE RAW WATER PUMPING-TDH=50
2,0.101,0.072,105.0,50.0
1,99,PACKAGE COMPLETE TREATMENT PLANT
2,0.101,0.072,70.0,50.0
3,5.0,GPM/SF
4,70.0,12.0,ALUM, 20 MG/L
5,4000.,0.15,POLYMER($2/LB),0.25 MG/L
6,300.0,1.8,CHLORINE, 3 MG/L
7,0.0,0.0,
1,126,STEEL BACKWASH/CLEARWELL TANKS
2,0.101,0.072,15000.0,15000.0
1,125,PACKAGE HIGH SERVICE PUMP STATN
2,0.101,0.072,105.0,50.0
1,131,SAND DRYING BEDS
2,0.101,0.072,500.0,500.0
```

***** COST ESTIMATE FOR PACKAGE RAW WATER PUMPING-TDH=50

	DESIGN	OPERATING
PROCESS FLOW	0.101 MGD	0.072 MGD
PROCESS PARAMETER	105.00 GPM	50.00 GPM
CAPITAL COST	DOLLARS	
CONSTRUCTION	15453.	
OTHER RELATED COSTS	5691.	
PROCESS CAPITAL COST	21344.	
O&M COST	CTS/1000 GAL TREATED	DOLLARS/YR
ELECTRICAL ENERGY @ \$ 0.030/KWH	0.662	174.
MAINTENANCE MATERIAL	0.237	62.
LABOR @ \$10.000/HR	2.043	537.
DIESEL FUEL @ \$ 0.450/GAL	0.000	0.
NATURAL GAS @ \$.0013/CU FT	0.000	0.
CHEMICALS	0.000	0.
PROCESS O&M COST	2.943	773.
COST SUMMARY		
O&M	2.943	773.
DEBT @ 20.0 YRS AND 7.0 %	7.666	2015.
PROCESS TOTAL COST	10.609	2788.

***** COST ESTIMATE FOR PACKAGE COMPLETE TREATMENT PLANT

	DESIGN	OPERATING
PROCESS FLOW	0.101 MGD	0.072 MGD
PROCESS PARAMETER	70.00 GPM	50.00 GPM
CAPITAL COST	DOLLARS	
CONSTRUCTION	87293.	
OTHER RELATED COSTS	31736.	
PROCESS CAPITAL COST	119029.	
O&M COST	CTS/1000 GAL TREATED	DOLLARS/YR
ELECTRICAL ENERGY @ \$ 0.030/KWH	6.637	1744.
MAINTENANCE MATERIAL	2.426	638.
LABOR @ \$10.000/HR	64.883	17051.
DIESEL FUEL @ \$ 0.450/GAL	0.000	0.
NATURAL GAS @ \$.0013/CU FT	0.000	0.
CHEMICALS	1.375	361.
PROCESS O&M COST	75.321	19794.
COST SUMMARY		
O&M	75.321	19794.
DEBT @ 20.0 YRS AND 7.0 %	42.753	11235.
PROCESS TOTAL COST	118.074	31030.

***** COST ESTIMATE FOR STEEL BACKWASH/CLEARWELL TANKS

PROCESS FLOW	DESIGN 0.101 MGD	OPERATING
PROCESS PARAMETER	15000.00 GAL	0.072 MGD 15000.00 GAL
CAPITAL COST		DOLLARS
CONSTRUCTION	14896.	
OTHER RELATED COSTS	5415.	
	<hr/>	
PROCESS CAPITAL COST	20311.	
O&M COST	CTS/1000 GAL TREATED	DOLLARS/YR
ELECTRICAL ENERGY @ \$ 0.030/KWH	0.000	0.
MAINTENANCE MATERIAL	0.000	0.
LABOR @ \$10.000/HR	0.000	0.
DIESEL FUEL @ \$ 0.450/GAL	0.000	0.
NATURAL GAS @ \$.0013/CU FT	0.000	0.
CHEMICALS	0.000	0.
	<hr/>	
PROCESS O&M COST	0.000	0.
COST SUMMARY		
O&M	0.000	0.
DEBT @ 20.0 YRS AND 7.0 %	7.295	1917.
	<hr/>	
PROCESS TOTAL COST	7.295	1917.

***** COST ESTIMATE FOR PACKAGE HIGH SERVICE PUMP STATION

PROCESS FLOW	DESIGN 0.101 MGD	OPERATING
PROCESS PARAMETER	105.00 GPM	0.072 MGD 50.00 GPM
CAPITAL COST		DOLLARS
CONSTRUCTION	11866.	
OTHER RELATED COSTS	4314.	
	<hr/>	
PROCESS CAPITAL COST	16181.	
O&M COST	CTS/1000 GAL TREATED	DOLLARS/YR
ELECTRICAL ENERGY @ \$ 0.030/KWH	0.819	215.
MAINTENANCE MATERIAL	0.118	31.
LABOR @ \$10.000/HR	3.973	1044.
DIESEL FUEL @ \$ 0.450/GAL	0.000	0.
NATURAL GAS @ \$.0013/CU FT	0.000	0.
CHEMICALS	0.000	0.
	<hr/>	
PROCESS O&M COST	4.910	1290.
COST SUMMARY		
O&M	4.910	1290.
DEBT @ 20.0 YRS AND 7.0 %	5.812	1527.
	<hr/>	
PROCESS TOTAL COST	10.722	2818.

***** COST ESTIMATE FOR SAND DRYING BEDS

	DESIGN	OPERATING
PROCESS FLOW	0.101 MGD	0.072 MGD
PROCESS PARAMETER	500.00 SQ FT	500.00 SQ FT
CAPITAL COST	DOLLARS	
CONSTRUCTION	3763.	
OTHER RELATED COSTS	1368.	
	-----	-----
PROCESS CAPITAL COST	5130.	
O&M COST	CTS/1000 GAL TREATED	DOLLARS/YR
ELECTRICAL ENERGY @ \$ 0.030/KWH	0.000	0.
MAINTENANCE MATERIAL	0.076	20.
LABOR @ \$10.000/HR	9.701	2549.
DIESEL FUEL @ \$ 0.450/GAL	0.068	18.
NATURAL GAS @ \$.0013/CU FT	0.000	0.
CHEMICALS	0.000	0.
	-----	-----
PROCESS O&M COST	9.845	2587.
COST SUMMARY		
O&M	9.845	2587.
DEBT @ 20.0 YRS AND 7.0 %	1.843	484.
	-----	-----
PROCESS TOTAL COST	11.688	3072.

***** TOTAL COST ESTIMATE FOR WATER TREATMENT PLANT

CAPITAL COST	DOLLARS
CONSTRUCTION SITWORK, INTERFACE PIPING, ROADS @ 5.0 %	133471. 6674. -----
TOTAL CONSTRUCTION COST	140145.
GEN CONTRACTOR OVERHEAD & PROFIT @ 12.0 %	16817. -----
SUBTOTAL	156962.
ENGINEERING @ 10.0 %	15696. -----
SUBTOTAL	172659.
LAND, 0.25 ACRES @ \$ 2000/ACRE	500.
LEGAL, FISCAL, & ADMINISTRATIVE	6057.
INTEREST DURING CONSTRUCTION	2780. -----
TOTAL CAPITAL COST	181995.

O&M COST	CTS/1000 GAL TREATED	DOLLARS/YR
ELECTRICAL ENERGY @ \$ 0.030/KWH	8.118	2133.
MAINTENANCE MATERIAL	2.858	751.
LABOR @ \$10.000/HR	80.601	21182.
DIESEL FUEL @ \$ 0.450/GAL	0.068	18.
NATURAL GAS @ \$.0013/CU FT	0.000	0.
CHEMICALS	1.375	361. -----
TOTAL O&M COST	93.020	24446.

COST SUMMARY

O&M	93.020	24446.
DEBT @ 20.0 YRS AND 7.0 %	65.369	17179. -----
TOTAL COST	158.389	41625.

PROCESS	COST SUMMARY FOR 5 WATER TREATMENT PROCESSES				COSTS-CTS/1000 GAL			
	FLOW-MGD DESIGN	ACTUAL	PROCESS PARAMETER DESIGN	OPERATING	CONSTR	CAPITAL	OM&M DEBT	TOTAL
1 PACKAGE RAW WATER PUMPING-TDH=50	0.101	0.072	105.0 GPM	50.0 GPM	15653.	21344.	2.943	7.666
2 PACKAGE COMPLETE TREATMENT PLANT	0.101	0.072	70.0 GPM	50.0 GPM	87293.	119029.	75.321	42.753
LOADING RATE = 5.0 GPM/SQ FT								
\$ 70.00/TON FOR ALUM, 20 MG/L								
\$ 4000.00/TON FOR POLYMER (\$2/LB), 0.25 MG/L								
\$ 300.00/TON FOR CHLORINE, 3 MG/L								
3 STEEL BACKWASH/CLEANWELL TANKS	0.101	0.072	15000.0 GAL	15000.0 GAL	14896.	20311.	0.000	7.295
4 PACKAGE HIGH SERVICE PUMP STATION	0.101	0.072	105.0 GPM	50.0 GPM	11866.	16181.	4.910	5.812
5 SAND DRYING BERS	0.101	0.072	500.0 SQ FT	500.0 SQ FT	3763.	5130.	9.845	11.683

	TOTAL Q&H:	MATERIALS, \$	LABOR, HR	DIESEL, GAL	NAT GAS, CU FT	CHEMICALS, \$
PROCESS Q&H	71113.	751.	2118.	40.	0.	361.
1	5803.	62.	54.	0.	0.	0.
2	58137.	638.	1705.	0.	0.	361.
3	0.	0.	0.	0.	0.	0.
4	7174.	31.	104.	0.	0.	0.
5	0.	20.	255.	40.	0.	0.
			TOTAL CAPITAL	181995.		
SITWORK, SUBSURFACE, STNBY POWER				6674.		
GEN CON OH & P, 12.0%				16817.		
ENGINEERING				15696.		
LAND, 0.25 ACRES				500.		
LEGAL, FISCAL, ADMIN				6057.		
INT RURING CONSTR				2780.		

COSTS PRESENTED ARE CURRENT AS OF OCTOBER 1978

CAPITAL COST FACTORS

UNIT COST FACTORS

COST INDEXES

=	10.00	ELECTRICITY, \$/KWH	=	0.03	EXCAVATION (ENR SKILLED LABOR) =	247.0
=	5.00	LABOR, \$/HR	=	10.00	MANUFACTURED EQUIP (BLS #114) =	221.3
=		DIESEL FUEL, \$/GAL	=	0.450	CONCRETE (BLS #132) =	221.1
=	0.00	NATURAL GAS, \$/CU FT	=	.0013	STEEL (BLS #101.3) =	262.1
=	7.00	BLDNG ENERGY USE, KWH/SQ FT/YR	=	102.6	LABOR (ENR SKILLED LABOR) =	247.0
=					PIPES & VALVES (BLS #114,201) =	236.4
=	20.00				ELECTRICAL & INSTR (BLS #117) =	167.5
=	0.25				HOUSING (ENR BUILDING COST) =	254.8
=	2000.00				PRODUCER PRICE INDEX =	199.7
					ENR CONSTRUCTION COST INDEX, 1967 BASE YR USED IN LIEU OF ABOVE INDEXES)	265.4

EXIT

COST.DAT File

Example 2

COSTS PRESENTED ARE CURRENT AS OF OCTOBER 1978
CAPITAL COST FACTORS (% OF CONSTRUCTION COST):

1 ENGINEERING(%)	=10.
2 SITWORK, INTERFACE PIPING(%)	=5.
3 SUBSURFACE CONSIDERATIONS(%)	=0.0
4 STANDBY POWER(%)	=0.0
5 INTEREST RATE(%)	=7.
6 NUMBER OF YEARS	=20.0
7 LAND COST, \$/ACRE	=2000.

UNIT COST FACTORS:

8 ELECTRICITY, \$/KWH	=.03
9 LABOR, \$/HR	=10.
10 DIESEL FUEL, \$/GAL	=.45
11 NATURAL GAS, \$/CU FT	=.0013
12 BLDNG ENERGY USE,KWH/SQ FT/YR	=102.6

COST INDEXES:

13 EXCAVATION(ENR SKILLED LABOR)	=247.0
14 MANUFACTURED EQUIP (BLS #114)	=221.3
15 CONCRETE (BLS #132)	=221.1
16 STEEL (BLS #101.3)	=262.1
17 LABOR (ENR SKILLED LABOR)	=247.0
18 PIPE & VALVES (BLS #114.901)	=236.4
19 ELECTRICAL & INSTR (BLS #117)	=167.5
20 HOUSING (ENR BUILDING COST)	=254.76
21 PRODUCER PRICE INDEX	=199.7
22 ENR CONSTRUCTION, '67 BASE YR	=0.0
OUTPUT(4 FOR LP,5 FOR TELETYPE)	=5
PRINTOUT(DETAILED OR SUMMARY)	=SUMMARY

PROCESS.DAT File

Example 2

COST SUMMARY FOR 17 WATER TREATMENT PROCESSES

PROCESS	FLOW-MGD	DESIGN ACTUAL	PROCESS DESIGN	PARAMETER OPERATING	CONSTR	COSTS-DOLLARS CAPITAL	0&H	COSTS-CTS/1000 GAL DEBT TOTAL
1 ALUM FEED-LIQUID STOCK	40.000	28.000	556.0 LB/HR	350.0 LB/HR	71458.	98070.	1.071	0.091 1.161
2 SODIUM HYDROXIDE FEED SYSTEMS	40.000	28.000	5000.0 LB/DAY	3300.0 LB/DAY	47300.	64933.	1.209	0.060 1.269
3 POLYMER FEED SYSTEMS	40.000	28.000	67.0 LB/DAY	45.0 LB/DAY	22403.	30755.	0.352	0.038 0.381
4 RAPID MIX, G=600	40.000	28.000	2785.0 CU FT	2785.0 CU FT	44214.	60697.	0.133	0.056 0.189
5 FLOCCULATION-HORIZ PADDLE, G=50	40.000	28.000	13000.0 CU FT	13000.0 CU FT	81352.	111790.	0.029	0.103 0.132
6 RECL CLARIFIER-FECL3 & ALUM SLG	40.000	28.000	4444.0 SQ FT	4444.0 SQ FT	2247326.	3085128.	0.544	2.849 3.394
7 GRAVITY FILTRATION STRUCTURE	40.000	28.000	5560.0 SQ FT	5560.0 SQ FT	1747729.	2399281.	0.843	2.216 3.059
8 FILTRATION MEDIA-MIXED MEDIA	40.000	28.000	5560.0 SQ FT	5560.0 SQ FT	14895.	203441.	0.000	0.188 0.188
9 HYDRAULIC SURFACE WASH SYSTEMS	40.000	28.000	5560.0 SQ FT	5560.0 SQ FT	16054.	220820.	0.057	0.204 0.261
10 BACKWASH PUMPING FACILITIES	40.000	28.000	1001.0 GPM	5560.0 SQ FT	12234.	168214.	0.099	0.155 0.254
11 WASH WATER SURGE BASINS	40.000	28.000	200000.0 GAL	5560.0 SQ FT	357400.	49013.	0.000	0.453 0.453
12 CL2 FEED-CYLINDER STORAGE	40.000	28.000	670.0 LB/DAY	450.0 LB/DAY	68978.	94693.	0.362	0.087 0.450
13 CLEARWELL STORAGE-BELOW GROUND	40.000	28.000	2500000.0 GAL	2500000.0 GAL	912233.	1252038.	0.000	1.156 1.156
14 FINISHED WATER PUMPING FACILITY	40.000	28.000	55.0 MGD	28.0 MGD	415025.	567947.	1.526	0.526 2.052
15 GRAV SLDG THICKENER-ALUM & FECL3	40.000	28.000	850.0 SQ FT	850.0 SQ FT	73524.	10934.	0.018	0.093 0.111
16 BASKET CENTRIFUGES	40.000	28.000	115000.0 GPD	70000.0 GPD	334806.	458621.	0.981	0.425 1.406
17 DEWATERED SLUDGE HAULING ONE WAY MILES = 20.0	40.000	28.000	200000.0 CY/YR	120000.0 CY/YR	81507.	111893.	0.162	0.103 0.265
					TOTAL	693698.	9522972.	7.386 8.796 16.182
TOTAL O&M:	6927859.	MATERIALS,\$ 42554,	LABOR,HR 21708.	DIESEL,GAL 4816.	NAT GAS,CU FT 0.		CHEMICALS,\$ 285248.	
PROCESS O&M	1	46258.	96.	65.	0.	0.	107310.	
	2	46864.	253.	150.	0.	0.	120450.	
	3	26226.	303.	207.	0.	0.	32850.	
	4	284176.	58.	499.	0.	0.	0.	
	5	153594.	843.	164.	0.	0.	0.	
	6	70561.	10053.	4344.	0.	0.	0.	
	7	978196.	12173.	4464.	0.	0.	0.	
	8	76860.	0.	0.	0.	0.	0.	
	9	76860.	399.	310.	0.	0.	0.	
	10	132836.	3172.	294.	0.	0.	0.	

PROCESS & M	KWH	MATERIALS, \$	LABOR, HR	DIESEL, GAL	NAT GAS, CU FT	CHEMICALS, \$
11	0.	0.	0.	0.	0.	0.
12	79799.	2519.	747.	0.	0.	24637.
13	0.	0.	0.	0.	0.	0.
14	4687639.	4203.	1107.	0.	0.	0.
15	4138.	2229.	145.	0.	0.	0.
16	476762.	2998.	8300.	0.	0.	0.
17	0.	5254.	914.	4816.	0.	0.

COSTS PRESENTED ARE CURRENT AS OF OCTOBER 1978

CAPITAL COST FACTORS

ENGINEERING(%)	=	10.00	ELECTRICITY, \$/KWH	=	0.03	EXCAVATION (ENR SKILLED LABOR)=	247.0
SITE WORK, INTERFACE PIPING(%)	=	5.00	LABOR, \$/HR	=	10.00	MANUFACTURED EQUIP (BLS #114)=	221.3
SUBSURFACE CONSIDERATIONS(%)	=	0.00	DIESEL FUEL, \$/GAL	=	0.450	CONCRETE (BLS #132)	221.1
STANDBY POWER(%)	=	0.00	NATURAL GAS, \$/CU FT	=	.0013	STEEL (BLS #013)	262.1
INTEREST RATE(%)	=	7.00	BLDNG ENERGY USE, KWH/SQ FT/YR	=	102.6	LABOR (ENR SKILLED LABOR)	247.0
NUMBER OF YEARS	=	20.00				PIPES & VALVES (BLS #114, 201)	236.4
LAND AREA, ACRES	=	13.00				ELECTRICAL & INSTR (BLS #117)	167.5
LAND COST, \$/ACRE	=	2000.00				HOUSING (ENR BUILDING COST)	254.8

UNIT COST FACTORS

EXCAVATION (ENR SKILLED LABOR)=	247.0
MANUFACTURED EQUIP (BLS #114)=	221.3
CONCRETE (BLS #132)	221.1
STEEL (BLS #013)	262.1
LABOR (ENR SKILLED LABOR)	247.0
PIPES & VALVES (BLS #114, 201)	236.4
ELECTRICAL & INSTR (BLS #117)	167.5
HOUSING (ENR BUILDING COST)	254.8
PRODUCER PRICE INDEX	199.7

COST SUMMARY FOR 4 WATER TREATMENT PROCESSES

PROCESS	FLOW-HD DESIGN	ACTUAL	PROCESS PARAMETER DESIGN	OPERATING	CONSTR	COSTS-DOLLARS CAPITAL	COSTS-CTS/1000 GAL ORH	COSTS-CTS/1000 GAL DEBT TOTAL
1 REVERSE OSMOSIS \$.45.00/TON FOR SULFURIC ACID,25 MG/L \$.650.00/TON FOR SODIUM HEXA PO3.5 MG/L	5,000	3,500	5.0 MGD	3.5 MGD	2867035.	3893610.	44.717	28.769 73.486
2 CLEARWELL STORAGE-BELOW GROUND 3 CL2 FEED-CYLINDER STORAGE 4 FINISHED WATER PUMPING FACILITY	5,000	3,500	300000.0 GAL 63.0 LB/DAY	300000.0 GAL 44.0 LB/DAY	155098. 17884.	210485. 24271.	0.000 0.695	1.555 0.179 1.555
TBH = 200.0 FEET			3.5 MGD	3.5 MGD	85729.	116344.	1.850	0.860 2.710
			TOTAL		3127746.	4244710.	47.262	31.364 78.626
			SITEWORK,SUBSURFACE,STNBY POWER GEN CON OH & P, 10.0% ENGINEERING LAND, 1.50 ACRES LEGAL-FISCAL,ADMIN INT DURING CONSTR		156387. 328413. 361255. 3000. 37287. 230623.			
			TOTAL CAPITAL		4244710.			

TOTAL O&M:	KWH	MATERIALS,\$	LABOR,HR	DIESEL,gal	NAT GAS,CU FT	CHEMICALS,\$
	8915745.	263812.	3138.	0.	0.	41108.
PROCESS O&M						
1	8328984.	261476.	2121.	0.	0.	38699.
2	0.	0.	0.	0.	0.	0.
3	15851.	1634.	436.	0.	0.	2408.
4	570910.	702.	581.	0.	0.	0.

COSTS PRESENTED ARE CURRENT AS OF OCTOBER 1978

CAPITAL COST FACTORS		UNIT COST FACTORS		COST INDEXES	
ENGINEERING(%)	=	ELECTRICITY, \$/KWH	=	EXCAVATION (ENR SKILLED LABOR)	= 247.0
SITEWORK,INTERFACE PIPING(%)	=	LABOR, \$/HR	=	MANUFACTURED EQUIP (BLS #114)	= 221.3
SUBSURFACE CONSIDERATIONS(%)	=	DIESEL FUEL, \$/GAL	=	CONCRETE (BLS #132)	= 221.1
STANDBY POWER(%)	=	NATURAL GAS, \$/CU FT	=	STEEL (BLS #101.3)	= 262.1
INTEREST RATE(%)	=	BLDNG ENERGY USE,KWH/SQ FT/YR	=	LABOR(ENR SKILLED LABOR)	= 247.0
NUMBER OF YEARS	=	20.00	=	PIPES & VALVES (BLS #114,901)	= 236.4
LAND AREA, ACRES	=	1.50	=	ELECTRICAL & INSTR (BLS #117)	= 167.5
LAND COST, \$/ACRE	=	2000.00	=	HOUSING (ENR BUILDING COST)	= 254.8
				PRODUCER PRICE INDEX	= 199.7
				EXIT	

COST.DAT File

Example 3

COSTS PRESENTED ARE CURRENT AS OF OCTOBER 1978
CAPITAL COST FACTORS (% OF CONSTRUCTION COST):

1 ENGINEERING(%) =10.
2 SITEWORK, INTERFACE PIPING(%) =5.
3 SUBSURFACE CONSIDERATIONS(%) =0.0
4 STANDBY POWER(%) =0.0
5 INTEREST RATE(%) =7.
6 NUMBER OF YEARS =20.0
7 LAND COST, \$/ACRE =2000.

UNIT COST FACTORS:

8 ELECTRICITY, \$/KWH =.03
9 LABOR, \$/HR =10.
10 DIESEL FUEL, \$/GAL =.45
11 NATURAL GAS, \$/CU FT =.0013
12 BLDNG ENERGY USE,KWH/SQ FT/YR =102.6

COST INDEXES:

13 EXCAVATION(ENR SKILLED LABOR) =247.0
14 MANUFACTURED EQUIP (BLS #114) =221.3
15 CONCRETE (BLS #132) =221.1
16 STEEL (BLS #101.3) =262.1
17 LABOR (ENR SKILLED LABOR) =247.0
18 PIPE & VALVES (BLS #114.901) =236.4
19 ELECTRICAL & INSTR (BLS #117) =167.5
20 HOUSING (ENR BUILDING COST) =254.76
21 PRODUCER PRICE INDEX =199.7
22 ENR CONSTRUCTION, '67 BASE YR =0.0
OUTPUT(6 FOR LF,5 FOR TELETYPE) =5
PRINTOUT(DETAILED OR SUMMARY) =SUMMARY

9,2
7.5,12.5

PROCES.DAT File

Example 3

COST SUMMARY FOR 6 WATER TREATMENT PROCESSES

PROCESS	FLOW-MGD DESIGN ACTUAL	PROCESS DESIGN PARAMETER	OPERATING	CONSTR	DOLLARS CAPITAL	O&M	COSTS-CTS/1000 GAL DEBT TOTAL
1 IN-PLANT PUMPING TDH = 75.0 FEET	5,000 3.500	7.5 MGD	3.5 MGD	62492.	86482.	1.750	0.637 2,389
2 PRESSURE ION EXCHANGE-SOFTENING \$ 30.60/TON FOR GENERATION SALT	5,000 3.500	5.0 MGD	3.5 MGD	485446.	672081.	11.111	4.966 16,077
3 SODIUM HYDROXIDE FEED SYSTEMS \$ 200.00/TON FOR SODIUM HYDROXIDE, 15 MG/L	5,000 3.500	625.0 LB/DAY	438.0 LB/DAY	19182.	26546.	1.393	0.196 1,589
4 CL2 FEED-CYLINDER STORAGE \$ 300.00/TON FOR CHLORINE, 1.5 MG/L	5,000 3.500	63.0 LB/DAY	44.0 LB/DAY	17884.	24749.	0.695	0.183 0.878
5 CLEARWELL STORAGE-GROUND LEVEL 6 FINISHED WATER PUMPING FACILITY	5,000 3.500	500000.0 GAL 8.0 MGD	500000.0 GAL 3.5 MGD	128065. 85729.	177228. 118640.	0.000 1.850	1.310 0.877 2,727
TDH = 200.0 FEET							
				TOTAL	798998.	1105726.	16.799 8.170 24,969

SITEWORK, SUBSURFACE, STNBY POWER GEN CON OH & P, 12.0% ENGINEERING	100674.	39950.
LAND, 1.50 ACRES	93962.	
LEGAL, FISCAL, ADMIN	3000.	
INT DURING CONSTR	17677. 51464.	
TOTAL CAPITAL	1105726.	

PROCESS O&M:	KWH 1303682.	MATERIALS,\$ 18562.	LABOR,HR 4276.	DIESEL,GAL 0.	NAT GAS,CU FT 0.	CHEMICALS,\$ 114170.
PROCESS O&M						
1	527256.	680.	586.	0.	0.	0.
2	176604.	15393.	2548.	0.	0.	95774.
3	13061.	152.	126.	0.	0.	15987.
4	15851.	1634.	436.	0.	0.	2409.
5	0.	0.	0.	0.	0.	0.
6	570910.	702.	581.	0.	0.	0.

COSTS PRESENTED ARE CURRENT AS OF OCTOBER 1978

CAPITAL COST FACTORS		UNIT COST FACTORS		COST INDEXES	
ENGINEERING(%)	= 10.00	ELECTRICITY, \$/KWH	= 0.03	EXCAVATION (ENR SKILLED LABOR)=	247.0
SITESWORK, INTERFACE PIPING(%)	= 5.00	LABOR, \$/HR	= 10.00	MANUFACTURED EQUIP (BLS #114) =	221.3
SUBSURFACE CONSIDERATIONS(%)	= 0.00	DIESEL FUEL, \$/GAL	= 0.450	CONCRETE (BLS #132)	= 221.1
STANDBY POWER(%)	= 0.00	NATURAL GAS, \$/CU FT	= .0013	STEEL (BLS #101.3)	= 262.1
INTEREST RATE(%)	= 7.00	BLDG ENERGY USE, KWH/SQ FT/YR	= 102.6	LABOR (ENR SKILLED LABOR)	= 247.0
NUMBER OF YEARS	= 20.00			PIPES & VALVES (BLS #114.901)	= 236.4
LAND AREA, ACRES	= 1.50			ELECTRICAL & INST (BLS #117)	= 167.5
LAND COST, \$/ACRE	= 2000.00			HOUSING (ENR BUILDING COST)	= 254.8
				PRODUCER PRICE INDEX	= 199.7

COST SUMMARY FOR 1 WATER TREATMENT PROCESS

PROCESS	FLOW-HGD DESIGN ACTUAL	PROCESS PARAMETER DESIGN	OPERATING	COSTS-DOLLARS CONSTR CAPITAL	COSTS-CTS/1000 GAL O&M DEBT TOTAL
1 LIME FEED-NO RECALCINATION \$ 65.00/TON FOR LIME,25 MG/L	1.000 0.700	8.7 LB/HR	6.1 LB/HR	57002. 77513.	3,371 2,864 6,234

SITEWORK-SUBSURFACE,STNBY POWER GEN CON OH & P, 12.0Z ENGINEERING 6703, LAND, 0.00 ACRES LEGAL,FISCAL,ADMIN INT DURING CONSTR	TOTAL 57002.	77513.	3,371 2,864 6,234
TOTAL CAPITAL 77513.			

TOTAL O&M: KWH 25617. MATERIALS:\$ 710.	LABOR/HR \$40.	DIESEL/GAL 0.	NAT GAS,CU FT 0.	CHEMICALS,\$ 1737.
---	----------------	---------------	------------------	--------------------

COSTS FOR THE FOLLOWING PROCESSES HAVE BEEN EXTRAPOLATED. VALID RANGES FOR INPUT DATA ARE:

PROCESS	DESIGN RANGE	YOUR INPUT	OPERATING RANGE	YOUR INPUT
1 LIME FEED-NO RECALCINATION	10.0 TO 1000.0 LB/HR	8.7	10.0 TO 1000.0 LB/HR	6.1

COSTS PRESENTED ARE CURRENT AS OF OCTOBER 1978

CAPITAL COST FACTORS	UNIT COST FACTORS	COST INDEXES
ENGINEERING(%)	= 10.00 ELECTRICITY, \$/KWH	= 0.03 EXCAVATION (ENR SKILLED LABOR)= 247.0
SITEWORK,INTERFACE PIPING(%)	= 5.00 LABOR, \$/HR	= 10.00 MANUFACTURED EQUIP (BLS #114)= 221.3
SUBSURFACE CONSIDERATIONS(%)	= 0.00 DIESEL FUEL, \$/GAL	= 0.450 CONCRETE (BLS #132)= 221.1
STANDBY POWER(%)	= 0.00 NATURAL GAS, \$/CU FT	= .0013 STEEL (BLS #101.3)= 262.1
INTEREST RATE(%)	= 7.00 BLDG ENERGY USE,KWH/SQ FT/YR	= 102.6 LABOR(ENR SKILLED LABOR)= 247.0
NUMBER OF YEARS	= 20.00 PIPES & VALVES (BLS #14.901)= 236.4	
LAND AREA, ACRES	= 0.00 ELECTRICAL & INSTR (BLS #117)= 167.5	
LAND COST, \$/ACRE	= 2000.00 HOUSING (ENR BUILDING COST)= 254.8	
		PRODUCER PRICE INDEX = 199.7

COST SUMMARY FOR 6 WATER TREATMENT PROCESSES

PROCESS	FLOW-MGD	DESIGN ACTUAL	PROCESS DESIGN	PARAMETER OPERATING	COSTS-DOLLARS	COSTS-CTS/1000 GAL
					CONSTR CAPITAL	O&M DEBT TOTAL
1 IN-PLANT PUMPING TDH = 75.0 FEET	5,000	3,500	7.5 MGD	3.5 MGD	62492.	0.635 2,274
2 PRESSURE ION EXCHANGE-SOFTENING \$.30-.40/TON FOR REGENERATION SALT	5,000	3,500	5.0 MGD	3.5 MGD	485646.	4.966 15,578
3 SODIUM HYDROXIDE FEED SYSTEMS \$ 200.00/TON FOR SODIUM HYDROXIDE, 15 MG/L	5,000	3,500	625.0 LB/DAY	438.0 LB/DAY	19182.	0.196 1,564
4 CL2 FEED-CYLINDER STORAGE \$ 300.00/TON FOR CHLORINE, 1.5 MG/L	5,000	3,500	63.0 LB/DAY	44.0 LB/DAY	17884.	0.610 0.183 0.792
5 CLEARWELL STORAGE-GROUND LEVEL 6 FINISHED WATER PUMPING FACILITY	5,000	3,500	500000.0 GAL	500000.0 GAL	128065.	0.000 1.310 1.310
TDH = 200.0 FEET	5,000	3,500	8.0 MGD	3.5 MGD	85729.	0.877 2,613
					TOTAL	798998. 1105726. 15,962. 0.170 24,132

SITEMARK, SUBSURFACE STANBY POWER GEN CON OH & P, 12.0% ENGINEERING	39950.	LAND, 1.50 ACRES	100674.
LAND, 1.50 ACRES	93962.	LEGAL, FISCAL, ADMIN	3000.
LEGAL, FISCAL, ADMIN	17677.	INT DURING CONSTR.	51464.
INT DURING CONSTR.			
		TOTAL CAPITAL	1105726.

TOTAL O&M:	KWH	MATERIALS, \$	LABOR, HR	DIESEL, GAL	NAT GAS, CU FT	CHEMICALS, \$
PROCESS O&M						
1	\$27256.	18562.	4272.	0.	0.	114170.
2	176604.	680.	586.	0.	0.	0.
3	13061.	15393.	2548.	0.	0.	95774.
4	15851.	1522.	126.	0.	0.	15987.
5	0.	1634.	436.	0.	0.	2409.
6	570910.	0.	0.	0.	0.	0.
		702.	581.	0.	0.	0.

COSTS PRESENTED ARE CURRENT AS OF OCTOBER 1978

CAPITAL COST FACTORS	UNIT COST FACTORS	COST INDEXES
ENGINEERING(%)	= 10.00 ELECTRICITY, \$/KWH	= 0.03 EXCAVATION (ENR SKILLED LABOR) = 247.0
SITEMARK, INTERFACE FITTING (%)	= 5.00 LABOR, \$/HR	= 7.50 MANUFACTURED EQUIP (BLS #114) = 221.3
SITESURFACE CONSIDERATIONS (%)	= 0.00 DIESEL FUEL, \$/GAL	= 0.450 CONCRETE (BLS #112) = 222.1
STANDBY POWER (%)	= 0.00 NATURAL GAS, \$/CU FT	= .0013 STEEL (BLS #101.3) = 262.1
INTEREST RATE (%)	= 7.00 BUILDING ENERGY USE, KWH/SQ FT/YR	= 102.6 LABOR (ENR SKILLED LABOR) = 247.0
NUMBER OF YEARS	= 20.00	= 102.6 PIPES & VALVES (BLS #114.901) = 236.4
LAND AREA, ACRES	= 1.50	= 1.50 ELECTRICAL & INSTR (BLS #117) = 167.5
LAND COST, \$/ACRE	= 2000.00	= 2000.00 HOUSING (ENR BUILDING COST) = 251.8
		= 2000.00 PRODUCER PRICE INDEX = 199.7

COST SUMMARY FOR 1 WATER TREATMENT PROCESS

PROCESS	FLOW-HGD	DESIGN ACTUAL	PROCESS PARAMETER	CONSTR	COSTS-DOLLARS CAPITAL	COSTS-CTS/1000 GAL
			DESIGN	OPERATING	02H	DEBT
1 LIME FEED-NO RECALCINATION	1.000	0.700	8.7 LB/HR	6.1 LB/HR	57002.	77513.
\$ 65.00/TON FOR LIME, 25 HG/L						2.864
				TOTAL	57002.	77513.
					2.864	5.706

SITELWORK, SUBSURFACE, STNBY POWER	2850.
GEN CON OH & P, 12.0%	7182.
ENGINEERING	6703.
LAND, 0.00 ACRES	0.
LEGAL, FISCAL, ADMIN	3022.
INT DURING CONSTR	752.
TOTAL CAPITAL	77513.

TOTAL O&H:	KWH	MATERIALS,\$	LABOR,HR	DIESEL,GAL	NAT GAS,CU FT	CHEMICALS,\$
	25617.	710.	540.	0.	0.	1737.

COSTS FOR THE FOLLOWING PROCESSES HAVE BEEN EXTRAPOLATED. VALID RANGES FOR INPUT DATA ARE:

PROCESS	DESIGN RANGE	YOUR INPUT	OPERATING RANGE	YOUR INPUT
1 LIME FEED-NO RECALCINATION	10.0 TO 1000.0 LB/HR	8.7	10.0 TO 1000.0 LB/HR	6.1

COSTS PRESENTED ARE CURRENT AS OF OCTOBER 1978

CAPITAL COST FACTORS	UNIT COST FACTORS	COST INDEXES
ENGINEERING(%)	ELECTRICITY, \$/KWH	0.03
SITELWORK, INTERFACE PIPING (%)	LABOR, \$/HR	= 7.50
SUBSURFACE CONSIDERATIONS (%)	DIESEL FUEL, \$/GAL	= 0.450
STANDBY POWER (%)	NATURAL GAS, \$/CU FT	= .0013
INTEREST RATE (%)	BLDG ENERGY USE,KWH/SQ FT/YR	= .01.3
NUMBER OF YEARS		= 102.6
LAND AREA, ACRES		= 247.0
LAND COST, \$/ACRE		= 236.4
		= 221.3
		= 221.1
		= 265.1
		= 247.0
		= 236.4
		= 167.5
		= 254.8
		= 199.7

COST SUMMARY FOR 6 WATER TREATMENT PROCESSES

PROCESS	FLOW-MGD DESIGN ACTUAL	PROCESS PARAMETER DESIGN	COSTS-\$/DOLLARS CONSTR	COSTS-\$/DOLLARS CAPITAL	COSTS-CTS/\$1000 GAL 0.8M	COSTS-CTS/\$1000 GAL DEBT	TOTAL
1 IN-PLANT PUMPING TDH = 75.0 FEET	5,000	3,500	7.5 MGD	3.5 MGD	62492.	86482.	1,639
2 PRESSIONATION SALT \$.30-.60/TON FOR REGENERATION SALT	5,000	3,500	5.0 MGD	3.5 MGD	485446.	672081.	11,410
3 SODIUM HYDROXIDE FEED SYSTEMS \$.200.00/TON FOR SODIUM HYDROXIDE, 15 MG/L	5,000	3,500	625.0 LB/DAY	438.0 LB/DAY	19182.	265446.	1,418
4 CL2 FEED-CYLINDER STORAGE \$.300.00/TON FOR CHLORINE, 1.5 MG/L	5,000	3,500	63.0 LB/DAY	44.0 LB/DAY	17884.	24749.	.780
5 CLEARWELL STORAGE-GROUND LEVEL TDH = 200.0 FEET	5,000	3,500	500000.0 GAL	500000.0 GAL	128945.	177226.	0.000
6 FINISHED WATER PUMPING FACILITY	5,000	3,500	8.0 MGD	3.5 MGD	85729.	118640.	1,964

16110 2988888 11105736 112-636 8-170 25-806

OWNER 112.8% 37.3%; 100.674;

93962+
SERING
1988

ADMIN 17677.

ANSWERED
JULY 14, 1884.

HOSPITAL 1105726.

NAT GAS, CUP FL CHEMICALS, \$ 110170

88

95774.
15002

0. 2409.

ప్రాణికాల

COST INDEXES

0.03 EXCAVATION (ENR SKILLED LABOR) = 247.0

MANUFACTURED EQUIP (BLS #114) = 221.3
CONCRETE (BLS #172) = 221.1

.0013 STEEL (BLS #101.3) = 262.1

LABOUR & SKILLED LABOUR = 241.0
PIPES & VALVES (BL-S #114-201) = 236.4

ELECTRICAL & INSTR (BLS #117) = 167.5
HOUSING (BLS #117) = 854.5

PRODUCER PRICE INDEX = 199.7

SOCIAL RECENTED ARE CURRENT AS OF OCTOBER 1978

	TOTAL O&M:	KWH	MATERIALS:\$	LABOR,HR	DIESEL,GAL	NAT GAS,CU FT	CHEMICALS,\$
PROCESS O&M		1303682.	18562.	4276.	0.	0.	114170.
1	522756.	680.	586.	0.	0.	0.	0.
2	176604.	15393.	2548.	0.	0.	0.	95774.
3	13061.	152.	126.	0.	0.	0.	15987.
4	15851.	1634.	436.	0.	0.	0.	2409.
5	0.	0.	0.	0.	0.	0.	0.
6	570910.	702.	581.	0.	0.	0.	0.

55

COST SUMMARY FOR 1 WATER TREATMENT PROCESS

PROCESS	FLOW-MGD DESIGN ACTUAL	PROCESS PARAMETER DESIGN	OPERATING	CONSTR	COSTS-DOLLARS CAPITAL	COSTS-CCTS/1000 GAL D&H	COSTS-CCTS/1000 GAL DEBT	TOTAL
1 LIME FEED-NO RECALCINATION \$ 65.00/TON FOR LIME, 25 HQ/L	1.000 0.700	8.7 LB/HR	6.1 LB/HR	57002.	77513.	3.899	2.864	6.762

SITWORK, SUBSURFACE, STNBY POWER GEN CON DH & P, 12.0% ENGINEERING LAND, 0.00 ACRES LEGAL, FISCAL, ADMIN INT DURING CONSTR	2850. 7182, 6703, 0, 3022, 752,
TOTAL	57002.
TOTAL CAPITAL	77513.

TOTAL D&H:	KWH 25617.	MATERIALS,\$ 710.	LABOR, HR 540.	DIESEL, GAL 0.	NAT GAS, CU FT 0.	CHEMICALS,\$ 1737.
------------	---------------	----------------------	-------------------	-------------------	----------------------	-----------------------

COSTS FOR THE FOLLOWING PROCESSES HAVE BEEN EXTRAPOLATED. VALID RANGES FOR INPUT DATA ARE:

PROCESS	DESIGN RANGE 10.0 TO 1000.0 LB/HR	YOUR INPUT 8.7	OPERATING RANGE 10.0 TO 1000.0 LB/HR	YOUR INPUT 1000.0 LB/HR	YOUR INPUT 6.1
---------	--------------------------------------	-------------------	---	----------------------------	-------------------

COSTS PRESENTED ARE CURRENT AS OF OCTOBER 1978

CAPITAL COST FACTORS	UNIT COST FACTORS	COST INDEXES
ENGINEERING(%)	= 10.00 ELECTRICITY, \$/KWH	= 0.03 EXCAVATION (ENR SKILLED LABOR) = 247.0
SITWORK, INTERFACE PIPLING(%)	= 5.00 LABOR, \$/HR	= 12.50 MANUFACTURED EQUIP (BLS #114) = 222.3
SUBSURFACE CONSIDERATIONS(%)	= 0.00 DIESEL FUEL, \$/GAL	= 0.450 CONCRETE (BLS #132) = 221.1
STANDBY POWER(%)	= 0.00 NATURAL GAS, \$/CU FT	= .0013 STEEL (BLS #101.3) = 262.1
INTEREST RATE(%)	= 7.00 BLDG ENERGY USE, KWH/SQ FT/YR	= 102.6 LABOR (ENR SKILLED LABOR) = 247.0
NUMBER OF YEARS	= 20.00 PIPES & VALVES (BLS #114.901) = 236.4	
LAND AREA, ACRES	= 0.00 ELECTRICAL & INSTR (BLS #117) = 167.5	
LAND COST, \$/ACRE	= 2000.00 HOUSING (ENR BUILDING COST) = 254.8	
		PRODUCER PRICE INDEX = 199.7
		EXIT

SECTION 7

TROUBLE SHOOTING GUIDE

The WATER program is designed to check the PROCES.DAT file before computing process costs to assure that all necessary data cards are present. If an error exists in this file, the program will print the type of error and the line number in which the error occurred. The program also checks the length of the COST.DAT file to assure that it contains either 28 or 30 cards. The following self-explanatory error messages are contained in the program:

1. FORTRAN read error in card ____ of the PROCES.DAT file. This card should contain the word "ACRES=" followed by a floating point number of 15 digits or less.
2. Error - card with "ACRES=" is missing or misspelled. Check card ____ of the PROCES.DAT file.
3. FORTRAN read error in card ____ of the PROCES.DAT file. This card should contain the integer 1 followed by a comma, the process number, and name.
4. Error - this should be the first data card of a process and should begin with the integer 1 in column 1. Check card ____ of the PROCES.DAT file.
5. Error in card ____ of the PROCES.DAT file. ____ is an invalid process number. Processes are numbered 1 through 28 in Table ____ of the program manual.
6. Error in card ____ of the PROCES.DAT file. Card number ____ was expected for process ____, which requires ____ cards of data.
7. Error - not enough data in the COST.DAT file; this file should have either 28 or 30 cards.

In addition to the error messages, the program also notifies the user when his input data exceed the valid range of the stored cost data. In this case, the computer extrapolates the stored data. See example 3 in Section 6 for a sample listing of this situation.

Errors may arise that will not cause an error message or program interruption if the required commas between the input data values are forgotten. In this case, erroneous input values will result. If this happens, check the PROCES.DAT file for required commas.

SECTION 8
WATER PROGRAM LISTING

The WATER program is written specifically for the DEC PDP-1170 IAS computing system. Because this FORTRAN program may not be compatible with all systems, it may be necessary to modify the opening and closing of data files. Also, FORMAT statements do not contain the Hollerith or H-conversion; instead they transmit alphanumeric data by enclosing it directly in quotation marks.

WATER PROGRAM

```

INTEGER O,REPEAT,REDO          1
REAL M,L,MAINT,LABOR,LFAFEE   2
LOGICAL DLIMIT,OLIMIT        3
DIMENSION TDH(10),TMILE1(10),GPMSF1(10),AMAKUP(10),          4
: AMGL(10),VAR(22),VARVAL(10),IRANGE(150),NP(150),APCENT(10) 5
DIMENSION NCHEM(75),CMNAM(75,3),CMCST(75),CMANT(75),ITYPE(150) 6
DIMENSION SAVE1(10)           7
DOUBLE PRECISION OUTPUT,PROCES,DETAILED,DXU,OXU,CMNAM,CHECK1,CHECK 8
DIMENSION CONSTR(150),ELECTR(150),MAINT(150),LABOR(150),          9
: DIESEL(150),GAS(150),CHEM(150),QD(150),QA(150),DPV(150),      10
: OPV(150),PROCAP(150),CTSTDM(150),CTSDEB(150),CTSTL(150),      11
: NUMUN(150),DXU(150),OXU(150)          12
DIMENSION C(4),E(4),M(4),L(4),D(4),G(4),F(8),B(4)          13
DIMENSION PROCES(150,4),CTS(150)          14
COMMON NUMUN,N/A/TOP,BOTTOM,C,B,CI/B/OTOP,OBOT,E,M,L,D,G,CR9 15
COMMON/C/ENGR,SITE,SUBSUR,STNBY,RATE,YEARS,CLAND,ELEC,          16
: HOURLY,FUEL,GASCST,ENFT,CI1,CI2,CI3,CI4,CI5,CI6,CI7,CI8,CI9, 17
: CI10          18
EQUIVALENCE (ENGR,VAR(1))          19
DATA IVV,RETAILED,CHECK1/O,'DETAILED','ACRES='/          20
OPEN(UNIT=1,NAME='COST.DAT',TYPE='OLD')          21
READ(1,100,END=240) ENGR,SITE,SUBSUR,STNBY,RATE,YEARS,CLAND 22
READ(1,101,END=240) ELEC,HOURLY,FUEL,GASCST,ENFT          23
READ(1,102,END=240) CI1,CI2,CI3,CI4,CI5,CI6,CI7,CI8,CI9,CI10 24
READ(1,103,END=240) O,OUTPUT          25
READ(1,105,END=450) IVN,IVV          26
IF(IVN.LE.0.OR.IVN.GT.22) GOTO 620          27
READ(1,106,END=240) (VARVAL(I1),I1=1,IVV)          28
450 IVV=IVV+1          29
CLOSE(UNIT=1)          30
DO 610 REDO=1,IVV          31
IF(REDO.GT.1) VAR(IVN)=VARVAL(REDO-1)          32
CR1=CI1/247.0          33
CR2=CI2/221.3          34
CR3=CI3/221.1          35
CR4=CI4/262.1          36
CR5=CI5/247.0          37
CR6=CI6/236.4          38
CR7=CI7/167.5          39
CR8=CI8/254.76          40
CR9=CI9/199.7          41
CR10=CI10/265.38         42
OPEN(UNIT=2,NAME='PROCES.DAT',TYPE='OLD')          43
NCASE=0          44
ILINE=0          45
198 ILINE=ILINE+1          46
READ(2,151,END=251,ERR=210) CHECK,ACRES          47
IF(CHECK.NE.CHECK1) GOTO 215          48
199 ILINE=ILINE+1          49
READ(2,152,END=250,ERR=220) NCHK,NP(1)          50
IF(NCHK.EQ.0.AND.ILINE.GT.3) GOTO 245          51
IF(NCHK.NE.1) GOTO 225          52
IF(NP(1).LE.0.OR.NP(1).GT.131) GOTO 230          53
IZ=1+(NP(1)-1)*5          54
OPEN(UNIT=3,NAME='CRV.DAT',TYPE='OLD',ACCESS='DIRECT',          55
: FORM='FORMATTED',ASSOCIATEVARIABLE=IZN)          56
READ(3'IZ,153) (PROCES(1,I1),I1=1,4),NCHEM(1),ITYPE(1)          57
CLOSE(UNIT=3)          58
.GOTO(200,200,201,201,201,201,201,201,201,200,201,202)ITYPE(1) 59
200 NCARD=2+NCHEM(1)          60
GOTO 203          61
201 NCARD=3+NCHEM(1)          62
GOTO 203          63
202 NCARD=4+NCHEM(1)          64
203 DO 205 I1=2,NCARD          65
ILINE=ILINE+1          66
READ(2,154,END=235,ERR=235) NCHK          67
IF(NCHK.NE.I1) GOTO 235          68
205 CONTINUE          69
GOTO 199          70
210 WRITE(0,370) ILINE          71
GOTO 1000          72
215 WRITE(0,371) ILINE          73
GOTO 1000          74
220 WRITE(0,372) ILINE          75
GOTO 1000          76
225 WRITE(0,373) ILINE          77
GOTO 1000          78
230 WRITE(0,374) ILINE,NP(1)          79
GOTO 1000          80

```

WATER PROGRAM (CONTINUED)

```

235 WRITE(0,375) ILINE,I1,NP(1),(PROCES(1,I2),I2=1,4),NCARD      81
      GOTO 1000
240 WRITE(0,376)
      GOTO 1000
245 NCASE=NCASE+1
      GOTO 198
250 NCASE=NCASE+1
251 CLOSE(UNIT=2)
      OPEN(UNIT=2,NAME='PROCES.DAT',TYPE='OLD')
      DO 600 REPEAT=1,NCASE
      ICHEM2=0
      ITDH=0
      IMILES=0
      IMAKUP=0
      IGPM=0
      IMGL=0
      IPCENT=0
      N=0
      IPAGE=0
      TCOST=0.0
      TCTSE=0.0
      TCTSM=0.0
      TCTSL=0.0
      TCTS=0.0
      TCTSG=0.0
      TCTSC=0.0
      TE=0.0
      TM=0.0
      TL=0.0
      TD=0.0
      TG=0.0
      TC=0.0
      SUM1=0.0
      SUM2=0.0
      SUM3=0.0
      SUM4=0.0
      SUM5=0.0
      READ(2,127) ACRES
500  READ(2,110,END=531) NP(N+1)
      IF(NP(N+1).LE.0) GOTO 531
      N=N+1
      READ(2,115) QD(N),QA(N),DPV(N),OPV(N)
      IZ= 1 + (NP(N)-1)*5
      OPEN(UNIT=3,NAME='CRV.DAT',TYPE='OLD',ACCESS='DIRECT',
      : FORM='FORMATTED',ASSOCIATEVARIABLE=IZN)
      READ(3'IZ,120)(PROCES(N,I1),I1=1,4),DXU(N),OXU(N),BOTTOM,TOP,
      : PROP,IRATIO,IEXP,NCHEM(N),ITYPE(N)
      READ(3'IZ+1 ,121) O,E
      READ(3'IZ+2 ,121) M,L
      READ(3'IZ+3 ,121) R,G
      READ(3'IZ+4 ,122) B,F
      CLOSE(UNIT=3)
      IF(ITYPE(N).EQ.4.OR.ITYPE(N).EQ.6) GOTO 501
      OBOT=BOTTOM*PROP
      OTOP=TOP*PROP
      GOTO 502
501  OBOT=PROP
      OTOP=IRATIO*(10.0**IEXP)
502  DLIMIT=DPV(N).LT.BOTTOM.OR.DPV(N).GT.TOP
      DLIMIT=OPV(N).LT.OBOT.OR.OPV(N).GT.OTOP
      RATIO=IRATIO*(10.0**IEXP)
      CI=F(1)*CR1 + F(2)*CR2 + F(3)*CR3 + F(4)*CR4 + F(5)*CR5 +
      : F(6)*CR6 + F(7)*CR7 + F(8)*CR8
      IF(CI.LT.0.01) CI=CR9
      IF(CR10.GT.0.0) CI=CR10
      CHEM(N)=0.0
      NUMUN(N)=1
      IRANGE(N)=0
      W1=DPV(N)**2
      W2=DPV(N)**3
      W3=OPV(N)**2
      W4=OPV(N)**3
      CTS(N)=QA(N)*3650.
      GOTO(505,505,504,525,505,505,505,550,505,505,505,504)ITYPE(N)
504  READ(2,110) NUMUN(N)

```

WATER PROGRAM (CONTINUED)

```

505 CONSTR(N)=(C(1)+C(2)*DPV(N)+C(3)*W1+C(4)*W2)*NUMUN(N)*CI      156
BLDEN =(B(1)+B(2)*DPV(N)+B(3)*W1+B(4)*W2)*ELEC*ENFT/102.6    157
ELECTR(N)=(E(1)+E(2)*OPV(N)+E(3)*W3+E(4)*W4)*NUMUN(N)*ELEC    158
MAINT(N) =(M(1)+M(2)*OPV(N)+M(3)*W3+M(4)*W4)*NUMUN(N)*CR9     159
LABOR(N) =(L(1)+L(2)*OPV(N)+L(3)*W3+L(4)*W4)*NUMUN(N)*HOURLY   160
DIESEL(N)=(D(1)+D(2)*OPV(N)+D(3)*W3+D(4)*W4)*NUMUN(N)*FUEL    161
GAS(N)  =(G(1)+G(2)*OPV(N)+G(3)*W3+G(4)*W4)*NUMUN(N)*GASCST   162
IF(DLIMIT) CALL DRANGE(CONSTR(N),BLDEN,DPV(N))                  163
IF(DLIMIT) CALL ORANGE(ELECTR(N),MAINT(N),LABOR(N),DIESEL(N),    164
: GAS(N),OPV(N))                                                 165
IF(DLIMIT.OR.OLIMIT) IRANGE(N)=1                                 166
ELECTR(N)=ELECTR(N)+BLDEN                                       167
GOTO(510,520,510,530,535,540,545,510,510,554,557) ITYPE(N)    168
C          **TYPE 1**
510 IF(NCHEM(N).EQ.0) GOTO 526                                  169
ICHEM1=ICHEM2+1                                              170
ICHEM2=ICHEM2+NCHEM(N)                                         171
DO 515 I1=ICHEM1,ICHEM2                                         172
READ(2,111) CMCST(I1),(CMNAM(I1,I2),I2=1,3)                 173
CMAMT(I1)=OPV(N)*RATIO*365./2000.                            174
CHEM(N)=CHEM(N)+CMCST(I1)*CMAMT(I1)                           175
C          **TYPE 10**
515 IF(ITYPE(N).EQ.10) CHEM(N)=CHEM(N)*2000.0                176
515 CONTINUE                                              177
GOTO 526                                                 178
C          **TYPE 2**
520 ICHEM1=ICHEM2+1                                              179
ICHEM2=ICHEM2+NCHEM(N)                                         180
DO 522 I1=ICHEM1,ICHEM2                                         181
READ(2,113) CMCST(I1),CMAMT(I1),(CMNAM(I1,I2),I2=1,3)       182
CMAMT(I1)=CMAMT(I1)*365./2000.                                183
522 CHEM(N)=CHEM(N)+CMCST(I1)*CMAMT(I1)                         184
GOTO 526                                                 185
C          **TYPE 4**
525 READ(2,110) NUMUN(N)                                         186
CONSTR(N)=(C(1)+C(2)*DPV(N)+C(3)*W1+C(4)*W2)*NUMUN(N)*CI    187
BLDEN=(B(1)+B(2)*DPV(N)+B(3)*W3+B(4)*W4)*ELEC*ENFT/102.6    188
IF(DLIMIT) CALL DRANGE(CONSTR(N),W1,DPV(N))                  189
ELECTR(N)=(E(1)+E(2)*OPV(N)+E(3)*W3+E(4)*W4)*ELEC            190
MAINT(N)=(M(1)+M(2)*OPV(N)+M(3)*W3+M(4)*W4)*CR9             191
LABOR(N)=(L(1)+L(2)*OPV(N)+L(3)*W3+L(4)*W4)*HOURLY          192
IF(OLIMIT) GOTO 527                                           193
GOTO 528                                                 194
527 ISAVE=NUMUN(N)                                             195
NUMUN(N)=1                                                 196
CALL ORANGE(ELECTR(N),MAINT(N),LABOR(N),DIESEL(N),    197
: GAS(N),OPV(N))                                              198
NUMUN(N)=ISAVE                                              199
TOP=OTOP                                              200
BOTTOM=OBOT                                              201
CALL DRANGE(W1,BLDEN,OPV(N))                                202
528 IF(DLIMIT.OR.OLIMIT) IRANGE(N)=1                          203
ELECTR(N)=ELECTR(N)+BLDEN                                     204
DIESEL(N)=0.0                                              205
GAS(N)=0.0                                                 206
CHEM(N)=0.0                                              207
GOTO 526                                                 208
C          **TYPE 5**
530 ITDH=ITDH+1                                              209
READ(2,123) TDH(ITDH)                                         210
BLDEN=BLDEN*102.6/ELEC/ENFT*CI                               211
ELECTR(N)=ELECTR(N)*TDH(ITDH)/D(1)                           212
DIESEL(N)=0.0                                              213
DENOM=D(1)-D(2)                                            214
SLOPE=(CONSTR(N)-BLDEN)/DENOM                             215
BEE=(D(1)*BLDEN-D(2)*CONSTR(N))/DENOM                      216
CONSTR(N)=SLOPE*TDH(ITDH) + BEE                            217
BLDEN=0.0                                                 218
GOTO 526                                                 219
C          **TYPE 6**
535 IMILES=IMILES+1                                         220
READ(2,123) TMILE1(IMILES)                                    221
TMILES=TMILE1(IMILES)                                         222
MAINT(N)=MAINT(N)*TMILES                                     223
IF(TMILES.LE.25.0) LABOR(N)=LABOR(N)*(0.4133*TMILES+5.867)  224
IF(TMILES.GT.25.0) LABOR(N)=LABOR(N)*(14.71+TMILES/17.0)    225
DIESEL(N)=DIESEL(N)*TMILES                                 226
CHEM(N)=0.0                                                 227
GOTO 526                                                 228

```

WATER PROGRAM (CONTINUED)

```

C      **TYPE 7**
540 IMILES=IMILES+1                                235
      READ(2,123) TMILE1(IMILES)
      TMILES=TMILE1(IMILES)
      ELECTR(N)=ELECTR(N)/ELEC*CI
      SLOPE=(ELECTR(N)-CONSTR(N))/35.0
      BEE=(40.0*CONSTR(N)-5.0*ELECTR(N))/35.0
      CONSTR(N)=SLOPE*TMILES + BEE
      IF(TMILES.LE.20) LABOR(N)=LABOR(N)*(0.667+0.0667*TMILES)
      IF(TMILES.GT.20) LABOR(N)=LABOR(N)*1.0+0.05*TMILES
      MAINT(N)=MAINT(N)*TMILES/5.0
      GAS(N)=0.0
      DIESEL(N)=DIESEL(N)*TMILES/5.0
      ELECTR(N)=0.0
      BLDEN=0.0
      CHEM(N)=0.0
      GOTO 526                                         251

C      **TYPE 8**
545 IMAKUP=IMAUP+1                                 252
      READ(2,123) AMAKUP(IMAKUP)
      ICHEM2=ICHEM2+1                                253
      READ(2,111) CMGST(ICHEM2),(CMNAM(ICHEM2,I1),I1=1,3)
      CMAMT(ICHEM2)=OPV(N)*RATIO*365./2000.*AMAUP(IMAKUP)/100.
      CHEM(N)=CMGST(ICHEM2)*CMAMT(ICHEM2)           255
      GOTO 526                                         256

C      **TYPE 9**
550 IGPM=IGPM+1                                   260
      READ(2,123) GPMSF1(IGPM)
      GPMSF=GPMSF1(IGPM)
      IF(GPMSF.EQ.0.0) GPMSF=2.0
      W1=DPV(N)/GPMSF                               261
      W2=W1**2                                     262
      W3=W1**3                                     263
      BOTTOM=BOTTOM/2.0                            264
      TOP=TDP/5.0                                  265
      DLIMIT=W1.LT.BOTTOM.OR.W1.GT.TOP            266
      CONSTR(N)=(C(1)+C(2)*W1+C(3)*W2+C(4)*W3)*CI
      BLDEN=(B(1)+B(2)*W1+B(3)*W2+B(4)*W3)*ELEC*ENFT/102.6
      IF(DLIMIT) CALL ORANGE(CONSTR(N),BLDEN,W1)    267
      W1=OPV(N)/GPMSF                               268
      W2=W1**2                                     269
      W3=W1**3                                     270
      ELECTR(N)=(E(1)+E(2)*W1+E(3)*W2+E(4)*W3)*ELEC
      MAINT(N)=(M(1)+M(2)*W1+M(3)*W2+M(4)*W3)*CR9
      LABOR(N)=(L(1)+L(2)*W1+L(3)*W2+L(4)*W3)*HOURLY
      OLIMIT=W1.LT.BOTTOM.OR.W1.GT.TOP             271
      IF(OLIMIT) CALL ORANGE(ELECTR(N),MAINT(N),LABOR(N),DIESEL(N),
      : GAS(N),W1)                                272
      IF(OLIMIT.OR.OLIMIT) IRANGE(N)=1
      ELECTR(N)=ELECTR(N)*GPMSF/2.0+BLDEN          273
      DIESEL(N)=0.0                                 274
      GAS(N)=0.0                                    275
      ICHEM1=ICHEM2+1                                276
      ICHEM2=ICHEM2+NCHEM(N)
      DO 548 I1=ICHEM1,ICHEM2
      READ(2,113) CMGST(I1),CMAMT(I1),(CMNAM(I1,I2),I2=1,3)
      CMAMT(I1)=CMAMT(I1)*365./2000.
      CHEM(N)=CHEM(N)+CMGST(I1)*CMAMT(I1)          277
      GOTO 526                                         278

C      **TYPE 11**
554 IMGL=IMGL+1                                   294
      READ(2,123) AMGL(IMGL)
      SAVE1(IMGL)=CONSTR(N)*AMGL(IMGL)/D(1)
      CONSTR(N)=0.0                                 295
      DIESEL(N)=0.0                                296
      GOTO 526                                         297

C      **TYPE 12**
557 IPCENT=IPCENT+1                             301
      READ(2,123) APCENT(IPCENT)
      CONSTR(N)=CONSTR(N)*APCENT(IPCENT)/100.
      ELECTR(N)=ELECTR(N)*APCENT(IPCENT)/100.
      MAINT(N)=MAINT(N)*APCENT(IPCENT)/100.
      LABOR(N)=LABOR(N)*APCENT(IPCENT)/100.
      DIESEL(N)=DIESEL(N)*APCENT(IPCENT)/100.
      GAS(N)=GAS(N)*APCENT(IPCENT)/100.
      CHEM(N)=0.0                                    302
      GOTO 526                                         303
      GOTO 526                                         304
      GOTO 526                                         305
      GOTO 526                                         306
      GOTO 526                                         307
      GOTO 526                                         308
      GOTO 526                                         309
      GOTO 526                                         310
      GOTO 526                                         311
      GOTO 526                                         312
526 TCOST=TCOST+CONSTR(N)
      GOTO 500                                         313

```

WATER PROGRAM (CONTINUED)

```

531 CSTSUB=SITE*TCOST/100. 314
CSTSIT=SBSUR*TCOST/100. 315
CSTSTN=STNBY*TCOST/100. 316
SUBTL1=TCOST + CSTSIT + CSTSTN 317
OHP=12. 318
IF(SUBTL1.GE.2.5E6.AND.SUBTL1.LT.10.E6) OHP=10. 319
IF(SUBTL1.GE.10.E6.AND.SUBTL1.LT.25.E6) OHP=9. 320
IF(SUBTL1.GE.25.E6) OHP=8.5 321
CSTOHP=OHP*SUBL1/100. 322
SUBTL2=CSTOHP + SUBL1 323
CSTENG=ENGRX*SUBL2/100. 324
SUBL3=CSTENG + SUBL2 325
CSTLND=AACRES*CLAND 326
IF(SUBL3.GT.1.E6) GOTO 551 327
IF(SUBL3.LE.0.0) GOTO 552 328
LFAFEE=60.0+0.0447*SUBL3-6.406E-8*SUBL3**2+3.673E-14*SUBL3**3 329
BR=SUBL3/1.E4 330
CSTINT=(1.75+.252*BR-2.105E-3*BR**2+9.013E-6*BR**3)/ 331
: 24.*RATE*SUBL3/100. 332
GOTO 555 333
551 LFAFEE=125570.+6.823E-4*SUBL3-115564.*EXP(-6.015E-8*SUBL3) 334
BR=SUBL3/1.E6 335
CSTINT=(16.03+1.02*BR-1.188E-2*BR**2+3.7E-5*BR**3)/ 336
: 24.*RATE*SUBL3/100. 337
GOTO 555 338
552 LFAFEE=0.0 339
CSTINT=0.0 340
555 TCAP=SUBL3 + CSTLND + LFAFEE + CSTINT 341
W1=(1.+RATE/100.) 342
DEBT=TCAP*RATE/100.*W1**YEARS/(W1**YEARS-1.) 343
IMGL=0 344
DO 570 I=1,N 345
IF(TCOST.LE.0.0) GOTO 556 346
GOTO 558 347
556 W2=0.0 348
GOTO 559 349
558 W2=CONSTR(I)/TCOST 350
559 PRDEBT=DEBT*W2 351
OTHER=(TCAP-TCOST)*W2 352
PROCAP(I)=CONSTR(I) + OTHER 353
CTSELE=ELECTR(I)/CTS(I) 354
CTSMAI=MAINT(I)/CTS(I) 355
CTSLAB=LABOR(I)/CTS(I) 356
CTS DIE=DIESEL(I)/CTS(I) 357
CTSGAS=GAS(I)/CTS(I) 358
CTS CHE=CHEM(I)/CTS(I) 359
CTS DER(I)=PRDEBT/CTS(I) 360
CTSTOM(I)=CTSELE+CTSMAI+CTSLAB+CTS DIE+CTSGAS+CTS CHE 361
IF(ITYPE(I).EQ.11) IMGL=IMGL+1 362
IF(ITYPE(I).EQ.11) CTSTOM(I)=SAVE1(IMGL)/CTS(I) 363
CTSTL(I)=CTS DER(I) + CTSTOM(I) 364
TOM=ELECTR(I)+MAINT(I)+LABOR(I)+DIESEL(I)+GAS(I)+CHEM(I) 365
IF(ITYPE(I).EQ.11) TOM=SAVE1(IMGL) 366
TOTAL=TOM + PRDEBT 367
TCTSE=TCTSE + CTSELE 368
TCTSM=TCTSM + CTSMAI 369
TCTSL=TCTSL + CTSLAB 370
TCTSD=TCTSD + CTS DIE 371
TCTSG=TCTSG + CTSGAS 372
TCTSC=TCTSC + CTS CHE 373
TE=TE + ELECTR(I) 374
TM=TM + MAINT(I) 375
TL=TL + LABOR(I) 376
TD=TD + DIESEL(I) 377
TG=TG + GAS(I) 378
TC=TC + CHEM(I) 379
SUM1=SUM1 + CTS DEB(I) 380
SUM2=SUM2 + CTSTOM(I) 381
SUM3=SUM3 + CTSTL(I) 382
SUM4=SUM4 + TOM 383
SUM5=SUM5 + TOTAL 384
IF(OUTPUT.NE.DETAILED) GOTO 570 385
IF(IPAGE.EQ.0) WRITE(0,300) 386
IF(IPAGE.EQ.0) IPAGE=2 387
IF(NUMUN(I).GT.1) GOTO 560 388
WRITE(0,301) (PROCES(I,I1),I1=1,4),BD(I),QA(I),DPV(I),DXU(I), 389
: DPV(I),DXU(I) 390
WRITE(0,302) CONSTR(I),OTHER,PROCAP(I) 391
GOTO 565 392

```

WATER PROGRAM (CONTINUED)

```

560 IF(NUMUN(N).EQ.0) GOTO 561          393
    QD(I)=QD(I)/NUMUN(I)
    QA(I)=QA(I)/NUMUN(I)
561 WRITE(0,303) (PROCES(I,I1),I1=1,4),NUMUN(I),QD(I),QA(I),DPV(I),
    : DXU(I),OPV(I),OXU(I)           394
    QD(I)=QD(I)*NUMUN(I)           395
    QA(I)=QA(I)*NUMUN(I)           399
    WRITE(0,304) NUMUN(I),CONSTR(I),OTHER,PROCAP(I),NUMUN(I)      400
565 WRITE(0,305) ELEC,CTSELE,ELECTR(I),CTSMAI,MAINT(I),HOURLY,
    : CTSLAB,LABOR(I),FUEL,CTS DIESEL(I)           401
    WRITE(0,306) GASCST,CTS GAS,GAS(I),CTS CHE, CHEM(I),CTSTOM(I),TOM   402
    WRITE(0,307) CTSTOM(I),TOM,YEARS,RATE,CTSDEB(I),PRDEBT,          403
    : CTSTL(I),TOTAL           405
    IPAGE=IPAGE-1           406
570 CONTINUE          407
    IF(OUTPUT.NE.DETAILED) GOTO 571          408
    WRITE(0,300)          409
    WRITE(0,308) TCOST,SITE,CSTSIT          410
    IF(SUBSUR.GT.0.) WRITE(0,309) SUBSUR,CSTSUB          411
    IF(STNBY.GT.0.) WRITE(0,310) STNBY,CSTSTN          412
    WRITE(0,311) SUBTL1,OH P,CSTOHP,SUBTL2,ENGR,CSTENG,SUBL3 413
    ICLAND=CLAND          414
    IF(ACRES.GT.0.) WRITE(0,312) ACRES,ICLAND,CSTLN D          415
    WRITE(0,313) LFAFEE,CSTINT,TCAP          416
    WRITE(0,314) ELEC,TCTSE,TE,TCTSM,TM,HOURLY,TCTSL,TL,FUEL,TCTSD,TD 417
    WRITE(0,315) GASCST,TCTS,G,TG,TCTSC,TC,SUM2,SUM4 418
    WRITE(0,316) SUM2,SUM4,YEARS,RATE,SUM1,DEBT,SUM3,SUM5 419
571 ICHEM2=0          420
    ITDH=0           421
    IMILES=0          422
    IMAKUP=0          423
    IGPM=0           424
    IMGL=0           425
    IPCENT=0          426
    I3=0           427
    WRITE(0,300)          428
    I3=I3+8          429
    IF(N.GT.1) GOTO 575          430
    WRITE(0,317)          431
    GOTO 578          432
575 WRITE(0,318) N          433
578 WRITE(0,319)          434
    DO 590 I=1,N          435
    IF(I3-45) 583,580,581          436
580 IF(N-I) 581,583,581          437
581 IF(I3-63.LT.0.AND.N-I-1.GT.0) GOTO 583          438
582 I3=0           439
    WRITE(0,300)          440
    WRITE(0,318) N          441
    WRITE(0,319)          442
    I3=I3+8          443
583 WRITE(0,320) I,(PROCES(I,I1),I1=1,4),QD(I),QA(I),DPV(I),DXU(I),
    : OPV(I),OXU(I),CONSTR(I),PROCAP(I),CTSTOM(I),CTSDEB(I),CTSTL(I) 444
    I3=I3+1          445
    GOTO(735,735,700,705,710,715,715,720,725,735,730,732)ITYPE(I) 446
700 WRITE(0,331) NUMUN(I)          447
    I3=I3+1          448
    GOTO 735          449
705 W3=DPV(I)*NUMUN(I)*7.48/QD(I)/694.44          450
    WRITE(0,332) W3          451
    W3=DPV(I)*NUMUN(I)          452
    WRITE(0,341) W3,NUMUN(I)          453
    I3=I3+3          454
    GOTO 735          455
710 ITDH=ITDH+1          456
    WRITE(0,333) TDH(ITDH)          457
    I3=I3+1          458
    GOTO 735          459
715 IMILES=IMILES+1          460
    WRITE(0,334) TMILE1(IMILES)          461
    I3=I3+1          462
    GOTO 735          463
720 IMAKUP=IMA KUP+1          464
    WRITE(0,335) AMAKUP(IMA KUP)          465
    I3=I3+1          466
    GOTO 735          467
725 IGPM=IGPM+1          468
    WRITE(0,336) GPMSF1(IGPM)          469
    I3=I3+1          470
    GOTO 735          471
                                         472

```

WATER PROGRAM (CONTINUED)

730 IMGL=IMGL+1	473
WRITE(0,337) AMGL(IMGL)	474
I3=I3+1	475
GOTO 735	476
732 IPCENT=IPCENT+1	477
WRITE(0,331) NUMUN(I)	478
WRITE(0,339) AFCENT(IPCENT)	479
I3=I3+2	480
GOTO 735	481
735 IF(NCHEM(I).EQ.0) GOTO 590	482
ICHEM1=ICHEM2+1	483
ICHEM2=ICHEM2+NCHEM(I)	484
DO 585 I2=ICHEM1,ICHEM2	485
IF(ITYPE(I).EQ.10) GOTO 584	486
IF(CMAN(I2).LE.0.0) GOTO 585	487
WRITE(0,321) CMCST(I2),(CMNAM(I2,I4),I4=1,3)	488
I3=I3+1	489
GOTO 585	490
584 WRITE(0,328) CMCST(I2),(CMNAM(I2,I4),I4=1,3)	491
I3=I3+1	492
585 CONTINUE	493
590 CONTINUE	494
WRITE(0,322) TCOST,TCAP,SUM2,SUM1,SUM3	495
I3=I3+4	496
SUM6=CSTSIT+CSTSUB+CSTSTN	497
WRITE(0,329) SUM6,OHP,CSTOHP,CSTENG,ACRES,CSTLND,LFAFEE,	498
: CSTINT,TCAP	499
I3=I3+11	500
TE=TE/ELEC	501
TL=TL/HOURLY	502
TD=TD/FUEL	503
TG=TG/GASCST	504
WRITE(0,330) TE,TM,TL,TD,TG,TC	505
I3=I3+3	506
IF(N-1.EQ.0) GOTO 7778	507
IF(I3-60.GT.0) WRITE(0,300)	508
WRITE(0,351)	509
I3=I3+2	510
DO 7777 I=1,N	511
IF(I3-63.LT.0) GOTO 7776	512
WRITE(0,300)	513
WRITE(0,354)	514
I3=3	515
7776 TMP1=ELECTR(I)/ELEC	516
TMP2=LABOR(I)/HOURLY	517
TMP3=DISEL(I)/FUEL	518
TMP4=GAS(I)/GASCST	519
WRITE(0,350) I,TMP1,MAINT(I),TMP2,TMP3,TMP4,CHEM(I)	520
7777 I3=I3+1	521
7778 I8=0	522
DO 592 I=1,N	523
592 I8=I8+IRANGE(I)	524
IF(I8.EQ.0) GOTO 593	525
IF(58-I3-I8.LT.0) WRITE(0,300)	526
IF(58-I3-I8.LT.0) I3=0	527
I8=0	528
593 DO 596 I=1,N	529
IF(IRANGE(I).EQ.0) GOTO 596	530
IF(I8.GT.0) GOTO 594	531
IF(I3-63.EQ.0) WRITE(0,300)	532
IF(I3-63.EQ.0) I3=0	533
WRITE(0,352)	534
I8=I8+1	535
I3=I3+4	536
594 IZ=1+(NP(I)-1)*5	537
OPEN(UNIT=3,NAME='CRV.DAT',TYPE='OLD',ACCESS='DIRECT',	538
: FORM='FORMATTED',ASSOCIATEVARIABLE=IZN)	539
READ(3'IZ,125) BOTTOM,TOP,PROP,IRATIO,IEXP	540
CLOSE(UNIT=3)	541
IF(ITYPE(I).EQ.4.OR.ITYPE(I).EQ.6) GOTO 597	542
OBOT=BOTTOM*PROP	543
OTOP=TOP*PROP	544
GOTO 595	545
597 OBOT=PROP	546
OTOP=IRATIO*(10.0**IEXP)	547
595 WRITE(0,353) I,(PROCES(I,I1),I1=1,4),BOTTOM,OTOP,DXU(I),DPV(I),	548
: OBOT,OTOP,DXU(I),DPV(I)	549
I3=I3+1	550

WATER PROGRAM (CONTINUED)

```

596 CONTINUE                                         551
OPEN(UNIT=1,NAME='COST.DAT',TYPE='OLD')
IF(I3.GT.47) WRITE(0,300)
READ(1,104) B,F
WRITE(0,323) B,F
WRITE(0,324) ENGR,ELEC,CI1,SITE,HOURLY,CI2
WRITE(0,325) SUBSUR,FUEL,CI3,STNBY,GASCST,CI4,RATE,ENFT,CI5
WRITE(0,326) YEARS,CI6,ACRES,CI7,CLAND,CI8,CI9
IF(CI10.GT.0.01) WRITE (0,327) CI10
CLOSE(UNIT=1)                                         555
597 CONTINUE                                         552
598 CLOSE(UNIT=2)                                     553
599 610 CONTINUE                                         554
600 GOTO 1000                                         555
601 620 WRITE(0,338) IVN
602 1000 STOP                                         556
603 100 FORMAT(//6(34X,F9.2/),34X,F9.2)             557
604 101 FORMAT(4(34X,F9.2/),34X,F9.2)              558
605 102 FORMAT(9(34X,F9.2/),34X,F9.2)              559
606 103 FORMAT(34X,11/34X,A8)                         560
607 104 FORMAT(4A4,8A4)                             561
608 105 FORMAT(I,I1)                                562
609 106 FORMAT(10F)                                 563
610 110 FORMAT(2X,I)                                564
611 111 FORMAT(2X,F3A8)                            565
612 113 FORMAT(2X,2F3A8)                           566
613 114 FORMAT(2X,I,F)                            567
614 115 FORMAT(2X,4F)                               568
615 120 FORMAT(4AB,2A6,3E9.2,I4,I2,I1,I2)          569
616 121 FORMAT(4E10.2,4E10.2)                      570
617 122 FORMAT(4E10.2,8F5.3)                       571
618 123 FORMAT(2X,F)                                572
619 125 FORMAT(44X,3E9.2,I4,I2)                     573
620 127 FORMAT(6X,F)                                574
621 151 FORMAT(A6,F)                                575
622 152 FORMAT(2I)                                 576
623 153 FORMAT(4A8,45X,I1,I2)                      577
624 154 FORMAT(I)                                 578
625 300 FORMAT(1H1)                                579
626 301 FORMAT(//' ***** COST ESTIMATE FOR '4AB//T48,'DESIGN/T66,
: 'OPERATING/T12,'PROCESS FLOW/T41,F10.3,' MGD/T61,F10.3,
: ' MGD/T12,'PROCESS PARAMETER/T41,F10.2,1X,A6,T61,F10.2,1X,A6/')
627 302 FORMAT(T8,'CAPITAL COST/T55,'DOLLARS'//
: T12,'CONSTRUCTION/T52,F11.0/T12,'OTHER RELATED COSTS/T52,F11.0/
: T53,'-----'/T30,'PROCESS CAPITAL COST/T52,F11.0//'
: T8,'O&M COST/T49,'CTS/1000 GAL TREATED/T81,'DOLLARS/YR//')
628 303 FORMAT(//' ***** COST ESTIMATE FOR',1X,4A8,' ('I3,' UNITS)'//'
: T47,'DESIGN/T63,'OPERATING'/'
: T12,'PROCESS FLOW (PER UNIT)'T41,F11.3,' MGD',T61,F11.3,' MGD'/
: T12,'PROCESS PARAMETER (PER UNIT)'T41,F11.2,1X,A6,T61,F11.2,
: 1X,A6/)
629 304 FORMAT(T8,'CAPITAL COST (TOTAL FOR'I3,' UNITS)'T55,'DOLLARS'//
: T12,'CONSTRUCTION/T52,F11.0/T12,'OTHER RELATED COSTS/T52,F11.0/
: T53,'-----'/T30,'PROCESS CAPITAL COST/T52,F11.0//'
: T8,'O&M COST (TOTAL FOR'I3,' UNITS)'T49,'CTS/1000 GAL TREATED'
: T81,'DOLLARS/YR//')
630 305 FORMAT(T12,'ELECTRICAL ENERGY @ $'F6.3,'/KWH/T53,F10.3,T79,
: F11.0/T12,'MAINTENANCE MATERIAL/T53,F10.3,T79,F11.0/
: T12,'LABOR @ $'F6.3,'/HR/T53,F10.3,T79,F11.0/
: T12,'DIESEL FUEL @ $'F6.3,'/GAL/T53,F10.3,T79,F11.0)
631 306 FORMAT(T12,'NATURAL GAS @ $'F6.4,'/CU FT/T53,F10.3,T79,F11.0/
: T12,'CHEMICALS/T53,F10.3,T79,F11.0/
: T53,'-----'/T80,'-----'/T34,
: 'PROCESS O&M COST/F13.3,T79,F11.0)
632 307 FORMAT(T8,'COST SUMMARY'//
: T12,'O&M/T52,F11.3,T79,F11.0/T12,'DEBT @'
: F5.1,' YRS AND F5.1,' %'T52,F11.3,T79 ,F11.0/
: T53,'-----'/T80,'-----'/
: T32,'PROCESS TOTAL COST/T52,F11.3,T79 ,F11.0)
633 308 FORMAT(//' ***** TOTAL COST ESTIMATE FOR WATER TREATMENT PLANT'
: //T8,'CAPITAL COST/T55,'DOLLARS'//
: T12,'CONSTRUCTION/T52,F11.0/
: T12,'SITWORK,INTERFACE PIPING,ROADS @'F5.1,' %'T52,F11.0)
634 309 FORMAT(T12,'SUBSURFACE CONSIDERATIONS @'F5.1,' %'T52,F11.0)
635 310 FORMAT(T12,'STANDBY POWER @'F5.1,' %'T52,F11.0)

```

WATER PROGRAM (CONTINUED)

```

311 FORMAT(T53,'-----'/T27,'TOTAL CONSTRUCTION COST' T52,F11.0//      626
: T12,'GEN CONTRACTOR OVERHEAD & PROFIT @'F5.1,' %'T55,F8.0/      627
: T53,'-----'/T42,'SUBTOTAL' T52,F11.0//      628
: T12,'ENGINEERING @'F5.1,' %'T52,F11.0/T53,'-----'/      629
: T42,'SUBTOTAL' T52,F11.0//      630
312 FORMAT(T12,'LAND',F7.2,' ACRES @ $'I6,'/ACRE' T52,F11.0)      631
313 FORMAT(T12,'LEGAL,FISCAL, & ADMINISTRATIVE' T52,F11.0/      632
: T12,'INTEREST DURING CONSTRUCTION' T52,F11.0/      633
: T53,'-----'/T32,'TOTAL CAPITAL COST' T52,F11.0//)      634
314 FORMAT(T8,'O&M COST' T49,'CTS/1000 GAL TREATED'      635
: T81,'DOLLARS/YR//      636
: T12,'ELECTRICAL ENERGY @ $'F6.3,'/KWH' T53,F10.3,T79,F11.0/      637
: T12,'MAINTENANCE MATERIAL' T53,F10.3,T79,F11.0/      638
: T12,'LABOR @ $'F6.3,'/HR' T53,F10.3,T79,F11.0/      639
: T12,'DIESEL FUEL @ $'F6.3,'/GAL' T53,F10.3,T79,F11.0)      640
315 FORMAT(T12,'NATURAL GAS @ $'F6.4,'/CU FT' T53,F10.3,T79,F11.0/      641
: T12,'CHEMICALS' T53,F10.3,T79,F11.0/      642
: T53,'-----'/T80,'-----'/T36,      643
: 'TOTAL O&M COST' F13.3 T79,F11.0//)      644
316 FORMAT(T8,'COST SUMMARY//      645
: T12,'O&M' T52,F11.3,T79,F11.0/T12,'DEBT @'      646
: F5.1,' YRS AND' F5.1,' %' T52,F11.3,T79,F11.0/      647
: T53,'-----'/T80,'-----'/      648
: T40,'TOTAL COST' T52,F11.3,T79,F11.0)      649
317 FORMAT(//T44,'COST SUMMARY FOR 1 WATER TREATMENT PROCESS')      650
318 FORMAT(//T44,'COST SUMMARY FOR I4,' WATER TREATMENT PROCESSES')      651
319 FORMAT(T17,'PROCESS' T42,'FLOW-MGD' T64,'PROCESS PARAMETER'      652
: T94,'COSTS-DOLLARS' T114,'COSTS-CTS/1000 GAL/'      653
: T40,'DESIGN ACTUAL' T61,'DESIGN' T76,'OPERATING' T92,'CONSTR'      654
: ,,' CAPITAL' T113,'O&M DEBT TOTAL')      655
320 FORMAT(1X,I2,1X,4A8,2F8.3,F11.1,1X,A6,F10.1,1X,A6,F10.0,F11.0,      656
: 3F8.3)      657
321 FORMAT(T7,'$',F7.2,'/TON FOR ',3A8)      658
322 FORMAT(T87,'-----//      659
: T82,'TOTAL' T88,F10.0,F11.0,3F8.3)      660
323 FORMAT(//1X,4A4,8A4/)      661
324 FORMAT(T11,'CAPITAL COST FACTORS' T58,'UNIT'      662
: ,,' COST FACTORS' T105,'COST INDEXES' //T5,'ENGINEERING(%)' T34,'='      663
: F8.2,T47,'ELECTRICITY, $/KWH' T80,'='F6.2,T91,'EXCAVATION'      664
: ,,' (ENR SKILLED LABOR)' =F7.1/T5,'SITWORK,INTERFACE PIPING(%)' =      665
: F8.2,T47,'LABOR, $/HR' T80,'='F6.2,T91,'MANUFACTURED EQUIP'      666
: ,,' (BLS #114)' =F7.1)      667
325 FORMAT(T5,'SUBSURFACE CONSIDERATIONS(%)' =F8.2,T47,'DIESEL'      668
: ,,' FUEL, $/GAL' T80,'='F6.3,T91,'CONCRETE (BLS #132)' T121,'='F7.1/      669
: T5,'STANDBY POWER(%)' T34,'='F8.2,T47,'NATURAL GAS, $/CU FT' T80,      670
: ' ='F6.4,T91,'STEEL (BLS #101.3)' T121,'='F7.1/T5,'INTEREST'      671
: ,,' RATE(%)' T34,'='F8.2,T47,'BLDG ENERGY USE,KWH/SQ FT/YR' T80,      672
: ' ='F6.1,T91,'LABOR(ENR SKILLED LABOR)' T121,'='F7.1)      673
326 FORMAT(T5,'NUMBER OF YEARS' T34,'='F8.2,T91,'PIPES & VALVES'      674
: ,,' (BLS #114.901)' =F7.1/T5,'LAND AREA, ACRES' T34,'='F8.2,T91,      675
: ' ELECTRICAL & INSTR (BLS #117)' =F7.1/T5,'LAND COST, $/ACRE'      676
: T34,'='F8.2,T91,'HOUSING (ENR BUILDING COST)' T121,'='F7.1/      677
: T91,'PRODUCER PRICE INDEX' T121,'='F7.1)      678
327 FORMAT(T47,'ENR CONSTRUCTION COST INDEX, 1967 BASE YR (USED IN'      679
: ' LIEU OF ABOVE INDEXES)' T121,'='F7.1)      680
328 FORMAT(T7,'$',F7.2,'/LB FOR ',3A8)      681
329 FORMAT(//T56,'SITWORK,SURFACE,STNBY POWER',T88,F10.0/T66,      682
: 'GEN CON OH & P',F5.1,'%',T88,F10.0/T76,'ENGINEERING',T88,F10.0/      683
: T69,'LAND',F7.2,' ACRES',T88,F10.0/      684
: T69,'LEGAL,FISCAL,ADMIN',T88,F10.0/T70,'INT DURING CONSTR',      685
: T88,F10.0/T87,'-----'/T74,'TOTAL CAPITAL',T88,F10.0)      686
330 FORMAT(// ' TOTAL O&M:',T21,'KWH',8X,'MATERIALS,$',9X,'LABOR,HR',      687
: 9X,'DIESEL,GAL',9X,'NAT GAS,CU FT',9X,'CHEMICALS,$'//      688
: T16,F11.0,5X,F10.0,8X,F9.0,0,9X,F10.0,9X,F13.0,10X,F10.0)      689
331 FORMAT(T7,'NUMBER OF UNITS =',I3)      690
332 FORMAT(T7,'EMPTY BED CONTACT TIME AT DESIGN FLOW =',F5.1,' MIN')      691
333 FORMAT(T7,'TBH =',F6.1,' FEET')      692
334 FORMAT(T7,'ONE WAY MILES =',F6.1)      693
335 FORMAT(T7,'MAKEUP LIME.=',F6.1,' %')      694
336 FORMAT(T7,'LOADING RATE =',F5.1,' GPM/SQ FT')      695
337 FORMAT(T7,'SLUDGE CONCENTRATION =',F8.0,' MG/L')      696
338 FORMAT(' PROGRAM EXIT. CHECK THE "COST.DAT" FILE',I6,' IS NOT'      697
: ' A VALID COST FACTOR NUMBER.')      698
339 FORMAT(T7,'COSTS CALCULATED FOR',F7.2,' % OWNERSHIP OF REGIONAL'      699
: ' FACILITY')      700
341 FORMAT(T7,'TOTAL VOL.=',F8.0,' CU FT (',I4,' CONTACTORS)')      701
350 FORMAT(1B,T16,F11.0,5X,F10.0,8X,F9.0,9X,      702
: F10.0,9X,F13.0,10X,F10.0)      703
351 FORMAT(// ' PROCESS O&M')      704

```

WATER PROGRAM (CONTINUED)

```

352 FORMAT('' COSTS FOR THE FOLLOWING PROCESSES HAVE BEEN' 705
: ' EXTRAPOLATED. VALID RANGES FOR INPUT DATA ARE:'// 706
: T17,'PROCESS',T43,'DESIGN RANGE',T69,'YOUR INPUT',T86, 707
: 'OPERATING RANGE',T114,'YOUR INPUT') 708
353 FORMAT(1X,I2,1X,4A8,F9.1,' TO',F11.1,1X,A6,F11.1,' TO', 709
: F11.1,1X,A6,F11.1) 710
354 FORMAT('' PROCESS O&M',T21,'KWH',8X,'MATERIALS,$',9X,'LABOR,HR', 711
: 9X,'DIESEL,GAL',9X,'NAT GAS,CU FT',9X,'CHEMICALS,$') 712
370 FORMAT('' FORTRAN READ ERROR IN CARD',I5,' OF THE PROCES.DAT FILE.' 713
: ' THIS CARD SHOULD CONTAIN THE WORD "ACRES" FOLLOWED BY'/
: ' A FLOATING POINT NUMBER OF 15 DIGITS OR LESS') 714
371 FORMAT('' ERROR-CARD WITH "ACRES" MISSING OR MISSPELLED.'/ 715
: ' CHECK CARD',I5,' OF THE PROCES.DAT FILE.') 716
372 FORMAT('' FORTRAN READ ERROR IN CARD',I5,' OF THE PROCES.DAT' 717
: ' FILE'// THIS CARD SHOULD CONTAIN THE INTEGER "1" / 718
: ' FOLLOWED BY'// A COMMA, THE PROCESS NUMBER AND THE PROCESS' 719
: ' NAME') 720
373 FORMAT('' ERROR-THIS SHOULD BE THE FIRST DATA CARD'// OF A' 721
: ' PROCESS AND SHOULD BEGIN WITH THE INTEGER "1" IN COLUMN 1'// 722
: ' CHECK CARD',I5,' OF THE PROCES.DAT FILE') 723
374 FORMAT('' ERROR IN CARD',I5,' OF THE PROCES.DAT FILE'//1X,I5, 724
: ' IS AN INVALID PROCESS NUMBER. PROCESSES'// ARE NUMBERED' 725
: ' 0 THRU 129 IN TABLE 2 OF THE PROGRAM MANUAL') 726
375 FORMAT('' ERROR IN CARD',I5,' OF THE PROCES.DAT FILE'// CARD' 727
: ' NO.',I3,' WAS EXPECTED FOR PROCESS',I4,1X,4A8,', WHICH' 728
: ' REQUIRES',I3,' CARDS OF DATA.') 729
376 FORMAT('' ERROR-NOT ENOUGH DATA IN THE COST.DAT FILE.'/ 730
: ' THIS FILE SHOULD HAVE EITHER 28 OR 30 CARDS') 731
END 732
SUBROUTINE DRANGE(Y1,Y2,X) 733
DIMENSION C(4),B(4),NUMUN(150),VAR(22) 734
COMMON NUMUN,N/A/TOP,BOTTOM,C,B,CI 735
COMMON/C/ENGR,SITE,SSUR,STNBY,RATE,YEARS,CLAND,ELEC, 736
: HOURLY,FUEL,GASCST,ENFT,CI1,CI2,CI3,CI4,CI5,CI6,CI7,CI8,CI9, 737
: CI10 738
EQUIVALENCE (ENGR,VAR(1)) 739
IF(X.LE.0.0) GOTO 98 740
GOTO 99 741
98 Y1=0.0 742
Y2=0.0 743
GOTO 130 744
99 IF(X-TOP.GT.0.0) GOTO 100 745
X1=BOTTOM 746
X2=2.*BOTTOM 747
GOTO 110 748
100 X1=TOP 749
X2=(TOP+BOTTOM)/2.0 750
110 C1=(C(1)+C(2)*X1+C(3)*X1**2+C(4)*X1**3) 751
C2=(C(1)+C(2)*X2+C(3)*X2**2+C(4)*X2**3) 752
B1= B(1)+B(2)*X1+B(3)*X1**2+B(4)*X1**3 753
B2= B(1)+B(2)*X2+B(3)*X2**2+B(4)*X2**3 754
ALX1=ALOG(X1) 755
ALX2=ALOG(X2) 756
DENOM=ALX2-ALX1 757
IF(C1.GT.0.0.AND.C2.GT.0.0) GOTO 115 758
Y1=0.0 759
GOTO 120 760
115 AC1=(ALOG(C1)*ALX2-ALOG(C2)*ALX1)/DENOM 761
AC2=(ALOG(C2)-ALOG(C1))/DENOM 762
Y1=EXP(AC1+AC2*ALOG(X))*NUMUN(N)*CI 763
120 IF(B1.GT.0.0.AND.B2.GT.0.0) GOTO 125 764
Y2=0.0 765
GOTO 130 766
125 AB1=(ALOG(B1)*ALX2-ALOG(B2)*ALX1)/DENOM 767
AB2=(ALOG(B2)-ALOG(B1))/DENOM 768
Y2=EXP(AB1+AB2*ALOG(X))*ELEC*ENFT/102.6 769
130 RETURN 770
END 771
SUBROUTINE ORANGE(Y1,Y2,Y3,Y4,Y5,X) 772
REAL M,L 773
DIMENSION E(4),M(4),L(4),B(4),G(4),NUMUN(150),VAR(22) 774
COMMON NUMUN,N/B/DTOP,OBOT,E,M,L,D,G,CR9 775
COMMON/C/ENGR,SITE,SSUR,STNBY,RATE,YEARS,CLAND,ELEC, 776
: HOURLY,FUEL,GASCST,ENFT,CI1,CI2,CI3,CI4,CI5,CI6,CI7,CI8,CI9, 777
: CI10 778
EQUIVALENCE(ENGR,VAR(1)) 779
F1(A1,A2)=(ALOG(A1)*ALX2-ALOG(A2)*ALX1)/DENOM 780
F2(A1,A2)=(ALOG(A2)-ALOG(A1))/DENOM 781
IF(X.LE.0.0) GOTO 98 782
GOTO 99 783

```

WATER PROGRAM (CONTINUED)

98	Y1=0.0	785
	Y2=0.0	786
	Y3=0.0	787
	Y4=0.0	788
	Y5=0.0	789
	GOTO 160	790
99	IF(X-OTOP.GT.0.0) GOTO 100	791
	X1=OBOT	792
	X2=2.0*OBOT	793
	GOTO 110	794
100	X1=OTOP	795
	X2=(OTOP+OBOT)/2.0	796
110	X12=X1**2	797
	X13=X1**3	798
	X22=X2**2	799
	X23=X2**3	800
	E1=E(1)+E(2)*X1+E(3)**X12+E(4)*X13	801
	E2=E(1)+E(2)*X2+E(3)**X22+E(4)*X23	802
	ALX2=ALOG(X2)	803
	ALX1=ALOG(X1)	804
	DENOM=ALX2-ALX1	805
	IF(E1.GT.0.0.AND.E2.GT.0.0) GOTO 115	806
	Y1=0.0	807
	GOTO 120	808
115	AE1=F1(E1,E2)	809
	AE2=F2(E1,E2)	810
	Y1=EXP(AE1+AE2*ALOG(X))*ELEC*NUMUN(N)	811
120	TM1=M(1)*M(2)*X1+M(3)*X12+M(4)*X13	812
	TM2=M(1)+M(2)*X2+M(3)*X22+M(4)*X23	813
	IF(TM1.GT.0.0.AND.TM2.GT.0.0) GOTO 125	814
	Y2=0.0	815
	GOTO 130	816
125	AM1=F1(TM1,TM2)	817
	AM2=F2(TM1,TM2)	818
	Y2=EXP(AM1+AM2*ALOG(X))*CR9*NUMUN(N)	819
130	TL1=L(1)+L(2)*X1+L(3)*X12+L(4)*X13	820
	TL2=L(1)+L(2)*X2+L(3)*X22+L(4)*X23	821
	IF(TL1.GT.0.0.AND.TL2.GT.0.0) GOTO 135	822
	Y3=0.0	823
	GOTO 140	824
135	AL1=F1(TL1,TL2)	825
	AL2=F2(TL1,TL2)	826
	Y3=EXP(AL1+AL2*ALOG(X))*HOURLY*NUMUN(N)	827
140	B1=D(1)+D(2)*X1+D(3)*X12+D(4)*X13	828
	D2=D(1)+D(2)*X2+D(3)*X22+D(4)*X23	829
	IF(B1.GT.0.0.AND.D2.GT.0.0) GOTO 145	830
	Y4=0.0	831
	GOTO 150	832
145	AD1=F1(D1,D2)	833
	AD2=F2(D1,D2)	834
	Y4=EXP(AD1+AD2*ALOG(X))*FUEL*NUMUN(N)	835
150	G1=G(1)+G(2)*X1+G(3)*X12+G(4)*X13	836
	G2=G(1)+G(2)*X2+G(3)*X22+G(4)*X23	837
	IF(G1.GT.0.0.AND.G2.GT.0.0) GOTO 155	838
	Y5=0.0	839
	GOTO 160	840
155	AG1=F1(G1,G2)	841
	AG2=F2(G1,G2)	842
	Y5=EXP(AG1+AG2*ALOG(X))*GASCST*NUMUN(N)	843
160	RETURN	844
	END	845

SECTION 9

CRV.DAT FILE

The CRV.DAT file contains all the cost information for the water treatment processes. The WATER program reads this file in a random or direct access mode. Each line of data contains 80 characters, so that if a record length of 80 is established on the system, the location of the first line of data of any process is given by:

$$(NP-1) \times 5 + 1$$

where NP is the number of the process shown in Table 4. For example, data for process 21, RAPID MIX, G=300, begins at line $(21-1) \times 5 + 1 = 101$ and continues through line 105. If the CRV.DAT is not established on the computing system as a random or direct access formatted file, the WATER program will have to be modified accordingly.

A copy of the CRV.DAT file is given on the following pages. The file is 655 lines long and contains 52,400 characters. Some systems may include a carriage return and line feed at the end of each line of data. In this case, the file will contain 82 characters per line and a total of 53,710. characters.

CRV.DAT FILE

CL2 FEED-CYLINDER STORAGE	LB/DAY	LB/DAY	1.00E+01	1.00E+04	1.00E+00	1	101
1.20E+04	9.43E+01	-1.44E-02	8.69E-07	5.45E+02	9.98E-01	7.14E-04	-5.05E-08
1.53E+03	2.39E+00	-4.38E-04	2.68E-08	4.01E+02	7.93E-01	-5.59E-05	2.66E-09
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
8.19E+03	1.13E+02	-1.22E-02	8.03E-07	0.00	0.50	0.00	0.00
CL2 FEED-ON SITE STORAGE TANK	LB/DAY	LB/DAY	2.00E+03	1.00E+04	1.00E+00	1	101
1.83E+05	-7.18E-01	1.97E-03	-7.97E-08	9.13E+02	1.84E-01	1.22E-04	-6.32E-09
4.15E+03	2.14E-01	3.55E-05	-1.61E-09	6.35E+02	1.92E-01	-2.55E-05	1.14E-09
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
-2.63E+02	3.23E+00	-3.15E-04	9.92E-09	0.00	0.81	0.00	0.02
CL2 FEED FROM RAIL CAR	LB/DAY	LB/DAY	2.00E+03	1.00E+04	1.00E+00	1	101
1.52E+05	2.44E+00	3.75E-04	1.94E-08	9.13E+02	1.84E-01	1.22E-04	-6.32E-09
4.15E+03	2.14E-01	3.55E-05	-1.61E-09	6.36E+03	3.80E-01	-4.92E-05	2.12E-09
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
-2.63E+02	3.23E+00	-3.15E-04	9.92E-09	0.00	0.82	0.00	0.00
CHLORINE DIOXIDE GENERATING,FEED	LB/DAY	LB/DAY	1.00E+01	3.50E+03	1.00E+00	17	1201
2.74E+04	2.55E+02	-7.17E-02	8.09E-06	2.94E+03	6.31E+00	2.61E-04	-8.13E-08
1.47E+03	5.30E+00	-1.70E-03	1.89E-07	5.88E+02	1.85E+00	-3.19E-04	2.99E-08
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
1.28E+04	6.80E+01	-2.20E-02	2.72E-06	0.00	0.41	0.00	0.00
OZONE GENERATION SYSTEMS	LB/DAY	LB/DAY	1.00E+01	3.50E+03	1.00E+00	1	1
4.12E+04	1.78E+03	-7.83E-01	1.31E-04	1.75E+04	3.33E+03	-6.98E-01	1.55E-04
1.26E+03	1.83E+01	-6.29E-03	9.52E-07	4.74E+02	1.06E+00	-1.37E-05	-2.61E-08
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
6.71E+03	1.60E+01	1.06E-02	-1.58E-06	0.00	0.79	0.00	0.00
OZONE CONTACT CHAMBER	CU FT	CU FT	4.60E+02	9.20E+04	1.00E+00	1	1
4.06E+03	4.93E+00	-1.04E-04	8.00E-10	0.00E+00	0.00E+00	0.00E+00	0.00E+00
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
ON-SITE HYPOCHLORITE GENERATION	LB/DAY	LB/DAY	1.00E+01	1.00E+04	1.00E+00	35	1101
1.58E+04	3.58E+02	-5.97E-02	3.37E-06	-4.90E+01	9.16E+02	-4.97E-03	3.67E-07
9.23E+02	1.06E+01	-9.70E-04	6.49E-08	3.76E+02	8.98E-01	-1.21E-04	6.59E-09
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
4.85E+03	8.09E+01	-1.50E-02	8.54E-07	0.00	0.60	0.00	0.21
ALUM FEED-LIQUID STOCK	LB/Hr	LB/Hr	5.40E+00	5.40E+03	1.00E+00	24	101
1.91E+04	1.14E+02	-3.86E-02	5.16E-06	3.24E+03	4.26E+00	1.80E-05	5.24E-07
7.38E+01	6.30E-02	4.15E-06	-1.17E-09	6.15E+01	6.92E-03	9.17E-06	-3.44E-10
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
5.43E+03	8.22E+01	-3.30E-02	3.32E-06	0.00	0.42	0.00	0.08
ALUM FEED-DRY STOCK	LB/Hr	LB/Hr	1.00E+01	5.00E+03	1.00E+00	24	101
2.09E+04	1.40E+02	-4.64E-02	7.40E-06	4.84E+03	2.28E+00	-7.93E-04	1.07E-07
1.99E+02	1.30E-01	4.46E-06	3.40E-09	2.68E+02	8.11E-01	2.87E-05	-4.02E-09
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
5.67E+03	9.81E+01	-3.57E-02	5.87E-06	0.00	0.40	0.00	0.03
POLYMER FEED SYSTEMS	LB/DAY	LB/DAY	1.00E+00	2.00E+02	1.00E+00	1	110
2.00E+04	1.73E+01	3.38E-01	-9.09E-04	1.73E+04	3.37E-03	1.05E-05	6.28E-08
2.59E+02	1.72E+00	-2.04E-02	8.58E-05	1.96E+02	3.33E-01	-2.16E-03	7.20E-06
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
7.99E+03	2.26E+01	-1.49E-01	4.68E-04	0.00	0.69	0.00	0.04
LIME FEED-NO RECALCINATION	LB/Hr	LB/Hr	1.00E+01	1.00E+03	1.00E+00	24	101
4.37E+04	2.84E+02	-4.56E-01	2.44E-04	3.25E+03	9.61E+00	-1.47E-02	7.94E-06
7.02E+02	2.52E+00	-4.47E-03	2.64E-06	5.20E+02	5.53E+00	-9.68E-03	5.68E-06
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
2.22E+04	1.67E+01	6.71E-02	-4.20E-05	0.00	0.53	0.00	0.02
LIME FEED-WITH RECALCINATION	LB/Hr	LB/Hr	1.00E+03	1.00E+04	1.00E+00	24	108
5.98E+04	2.30E+01	-3.54E-03	2.12E-07	1.35E+03	4.00E+00	-4.51E-04	3.34E-08
1.35E+03	-2.61E-03	1.30E-05	-7.11E-10	6.99E+02	1.47E+00	-1.76E-04	8.88E-09
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
1.63E+04	7.24E+00	-3.31E-04	8.73E-09	0.00	0.67	0.00	0.02
POTASSIUM PERMANGANATE FEED	LB/DAY	LB/DAY	1.00E+00	5.00E+02	1.00E+00	1	101
9.63E+03	2.41E+01	-4.69E-02	4.13E-05	3.08E+03	2.00E+00	1.54E-02	-1.17E-05
7.24E+01	3.48E-01	-6.92E-04	6.97E-07	2.06E+02	2.57E+00	-9.02E-03	1.03E-05
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
1.45E+03	1.61E+01	-4.65E-02	5.69E-05	0.00	0.33	0.00	0.06
SULFURIC ACID FEED SYSTEMS	GPD	GPD	1.00E+01	5.00E+03	1.00E+00	153	1101
8.60E+03	2.26E+01	-5.78E-03	7.24E-07	1.60E+03	-1.53E-01	2.54E-04	-3.15E-08
6.48E+01	4.90E-02	-1.46E-05	1.57E-09	7.88E+01	1.60E-01	-3.34E-05	4.67E-09
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
2.88E+03	-9.94E-01	3.52E-04	-3.79E-08	0.00	0.46	0.00	0.11
SODIUM HYDROXIDE FEED SYSTEMS	LB/DAY	LB/DAY	1.00E+01	1.00E+04	1.00E+00	1	101
1.44E+04	7.94E+00	-4.89E-04	4.34E-08	3.20E+03	8.66E-01	-3.39E-05	-2.79E-10
1.39E+02	2.86E-02	2.28E-06	-1.33E-10	1.20E+02	1.59E-02	-3.08E-06	3.03E-10
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
1.06E+03	1.47E+01	-2.03E-03	1.39E-07	0.00	0.39	0.00	0.05
FERROUS SULFATE FEED SYSTEMS	LB/Hr	LB/Hr	1.07E+01	5.35E+03	1.00E+00	24	101
1.96E+04	1.20E+02	-3.21E-02	4.61E-06	4.70E+03	2.09E+00	-5.59E-04	6.54E-08
1.85E+02	1.26E-01	-1.86E-05	6.45E-09	2.67E+02	7.95E-01	-4.06E-05	8.10E-09
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
5.71E+03	8.93E+01	-2.89E-02	4.44E-06	0.00	0.38	0.00	0.03

CRV.BAT FILE (CONTINUED)

FERRIC SULFATE FEED SYSTEMS LB/HR LB/HR 1.33E+01 6.60E+03 1.00E+00 24 101
 1.95E+04 9.79E+01 -2.26E-02 2.68E-06 4.79E+03 1.57E+00 -2.19E-04 1.46E-08
 1.88E+02 4.81E-02 3.59E-05 -2.62E-09 2.72E+02 5.38E-01 7.17E-05 -8.18E-09
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 5.80E+03 6.71E+01 -1.41E-02 1.76E-06 0.00 0.38 0.00 0.00 0.03 0.06 0.06 0.47
 ANHYDROUS AMMONIA FEED FACILITY LB/DAYLB/DAY 2.50E+02 5.00E+03 1.00E+00 1 101
 1.85E+04 5.70E+01 -1.68E-02 1.89E-06 -9.13E+01 3.41E+00 3.13E-03 -4.49E-07
 2.27E+03 2.48E+00 -6.03E-04 6.59E-08 4.57E+02 2.27E-01 -5.25E-05 5.71E-09
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 9.44E+03 2.53E+00 -1.05E-03 1.46E-07 0.00 0.55 0.00 0.00 0.15 0.10 0.11 0.09
 AQUA AMMONIA FEED FACILITY LB/DAYLB/DAY 2.50E+02 5.00E+03 1.00E+00 34-1101
 8.94E+03 1.58E+01 -3.50E-03 3.58E-07 5.70E+02 4.73E-07 -2.01E-10 1.69E-14
 3.99E+01 2.52E-01 -5.49E-05 5.43E-09 1.52E+02 1.26E-07 -5.51E-11 4.55E-15
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 POWDERED ACTIVATED CARBON FEED LB/HR LB/HR 3.50E+00 7.00E+03 1.00E+00 24 101
 7.01E+04 3.07E+02 -6.09E-02 5.35E-06 7.94E+03 1.36E+03 -3.62E-01 3.10E-05
 2.36E+03 2.00E+01 -3.67E-03 3.07E-07 9.29E+02 2.04E+00 -3.98E-04 4.50E-08
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 1.03E+04 7.39E-06 -4.71E-09 3.94E-13 0.01 0.44 0.02 0.04 0.05 0.15 0.24 0.05
 RAPID MIX, G=300 CU FT CU FT 1.00E+02 2.00E+04 1.00E+00 1 1
 1.38E+04 7.45E+00 2.16E-04 -4.63E-09 -9.19E-04 5.09E+01 -7.63E-10 1.48E-13
 2.05E+01 1.45E-02 -4.44E-07 2.21E-11 4.54E+02 -6.88E-03 9.09E-06 -2.95E-10
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 RAPID MIX, G=600 CU FT CU FT 1.00E+02 2.00E+04 1.00E+00 1 1
 1.41E+04 1.05E+01 1.15E-04 -9.31E-10 1.50E+01 1.02E+02 1.23E-05 -1.90E-10
 2.05E+01 1.45E-02 -4.44E-07 2.21E-11 4.54E+02 -6.88E-03 9.09E-06 -2.95E-10
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 RAPID MIX, G=900 CU FT CU FT 1.00E+02 2.00E+04 1.00E+00 1 1
 1.41E+04 1.99E+01 2.46E-05 1.90E-09 -7.51E+01 3.40E+02 -7.42E-05 2.91E-09
 2.05E+01 1.45E-02 -4.44E-07 2.21E-11 4.54E+02 -6.88E-03 9.09E-06 -2.95E-10
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 FLOCCULATION-HORIZ PADDLE, G=20 CU FT CU FT 1.80E+03 1.00E+06 1.00E+00 1 1
 3.40E+04 3.41E+00 -4.93E-06 3.32E-12 -2.55E+01 1.98E-01 -8.37E-09 8.71E-15
 3.66E+02 3.70E-02 -2.61E-08 1.77E-14 1.30E+02 2.68E-03 -5.51E-09 3.76E-15
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 FLOCCULATION-HORIZ PADDLE, G=50 CU FT CU FT 1.80E+03 1.00E+06 1.00E+00 1 1
 3.29E+04 3.80E+00 -5.18E-06 3.51E-12 -7.31E+01 1.19E+00 -1.71E-08 1.57E-14
 3.66E+02 3.70E-02 -2.61E-08 1.77E-14 1.30E+02 2.68E-03 -5.51E-09 3.76E-15
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 FLOCCULATION-HORIZ PADDLE, G=80 CU FT CU FT 1.80E+03 5.00E+05 1.00E+00 1 1
 2.82E+04 5.56E+00 -1.69E-05 2.25E-11 4.58E+01 3.36E+00 6.58E-09 -3.07E-14
 3.66E+02 3.70E-02 -2.61E-08 1.77E-14 1.30E+02 2.68E-03 -5.51E-09 3.76E-15
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 FLOCCULATION-VERT TURBINE, G=20 CU FT CU FT 1.80E+03 2.50E+04 1.00E+00 1 1
 1.11E+04 1.17E+01 -3.61E-04 4.46E-09 -2.55E+01 1.98E-01 -8.37E-09 8.71E-15
 3.66E+02 3.70E-02 -2.61E-08 1.77E-14 1.30E+02 2.68E-03 -5.51E-09 3.76E-15
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 FLOCCULATION-VERT TURBINE, G=50 CU FT CU FT 1.80E+03 2.50E+04 1.00E+00 1 1
 1.11E+04 1.17E+01 -3.61E-04 4.46E-09 -2.55E+01 1.98E-01 -8.37E-09 8.71E-14
 3.66E+02 3.70E-02 -2.61E-08 1.77E-14 1.30E+02 2.68E-03 -5.51E-09 3.76E-15
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 FLOCCULATION-VERT TURBINE, G=80 CU FT CU FT 1.80E+03 2.50E+04 1.00E+00 1 1
 1.04E+04 1.22E+01 -4.31E-04 6.92E-09 4.21E+01 3.37E+00 -2.54E-08 2.87E-14
 3.66E+02 3.70E-02 -2.61E-08 1.77E-14 1.30E+02 2.68E-03 -5.51E-09 3.76E-15
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 CIRCULAR CLARIFIER-LIME SLUDGE SQ FT SQ FT 7.07E+02 3.14E+04 1.00E+00 1 3
 5.83E+04 3.63E+01 -4.99E-04 6.35E-09 4.64E+03 4.18E-01 -2.09E-06 -4.35E-11
 1.01E+02 2.14E-01 -6.35E-06 1.14E-10 1.35E+02 2.24E-02 -6.61E-07 1.01E-11
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 RECTANGULAR CLARIFIER-LIME SLDG SQ FT SQ FT 2.40E+02 4.80E+03 1.00E+00 1 3
 2.38E+04 6.43E+01 -6.31E-03 7.38E-07 3.04E+03 9.62E-01 1.40E-04 1.40E-08
 2.53E+02 1.32E-01 -2.13E-06 3.64E-09 1.49E+02 8.61E-02 -4.09E-06 3.63E-10
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 RECT CLARIFIER-FECL3 % ALUM SLDG SQ FT SQ FT 2.40E+02 4.80E+03 1.00E+00 1 3
 2.38E+04 6.43E+01 -6.31E-03 7.38E-07 3.08E+03 8.15E-01 -4.68E-05 2.35E-08
 2.53E+02 1.32E-01 -2.13E-06 3.64E-09 1.49E+02 8.61E-02 -4.09E-06 3.63E-10
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00

CRV.DAT FILE (CONTINUED)

UPFLOW SOLIDS CONTACT CLAR,G=70 SQ FT SQ FT 2.55E+02 1.45E+04 1.00E+00 1 3
 6.59E+04 5.44E+01 -2.29E-03 2.52E-08 5.92E+03 8.73E+00 -2.79E-04 1.82E-08
 5.04E+02 2.71E-01 -1.57E-05 3.90E-10 4.23E+02 7.33E-02 -7.32E-06 2.47E-10
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.04 0.53 0.07 0.10 0.25 0.00 0.01 0.00
 UPFLOW SOLIDS CONTACT CLAR,G=110SQ FT SQ FT 2.55E+02 1.45E+04 1.00E+00 1 3
 6.59E+04 5.44E+01 -2.29E-03 2.52E-08 2.82E+03 2.09E+01 -1.32E-03 8.80E-08
 5.04E+02 2.71E-01 -1.57E-05 3.90E-10 4.23E+02 7.33E-02 -7.32E-06 2.47E-10
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.04 0.53 0.07 0.10 0.25 0.00 0.01 0.00
 UPFLOW SOLIDS CONTACT CLAR,G=150SQ FT SQ FT 2.55E+02 1.45E+04 1.00E+00 1 3
 6.59E+04 5.44E+01 -2.29E-03 2.52E-08 7.68E+03 2.22E+01 2.14E-03 -1.15E-07
 5.04E+02 2.71E-01 -1.57E-05 3.90E-10 4.23E+02 7.33E-02 -7.32E-06 2.47E-10
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.04 0.53 0.07 0.10 0.25 0.00 0.01 0.00
 TUBE SETTLING MODULES SQ FT SQ FT 2.80E+02 5.60E+04 1.00E+00 1 1
 2.86E+03 2.55E+01 -2.00E-04 1.91E-09 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00 0.50 0.00 0.33 0.17 0.00 0.00 0.00
 GRAVITY FILTRATION STRUCTURE SQ FT SQ FT 1.40E+02 2.80E+04 1.00E+00 1 1
 1.16E+05 3.92E+02 -2.04E-02 4.82E-07 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 4.31E+02 2.78E+00 -1.37E-04 3.03E-09 8.46E+02 8.04E-01 -3.28E-05 9.39E-10
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 1.72E+04 1.93E+02 -4.11E-03 8.71E-08 0.01 0.16 0.07 0.05 0.24 0.24 0.07 0.16
 FILTRATION MEDIA-RAPID SAND SQ FT SQ FT 3.70E+02 7.48E+04 1.00E+00 1 1
 3.80E+03 7.99E+00 -3.52E-05 3.78E-10 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00
 FILTRATION MEDIA-DUAL MEDIA SQ FT SQ FT 1.40E+02 2.99E+04 1.00E+00 1 1
 2.82E+03 2.03E+01 -7.01E-04 1.68E-08 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00
 FILTRATION MEDIA-MIXED MEDIA SQ FT SQ FT 1.40E+02 2.99E+04 1.00E+00 1 1
 4.68E+03 2.91E+01 -6.82E-04 1.63E-08 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00
 BACKWASH PUMPING FACILITIES GPM SQ FT 1.26E+03 2.30E+04 1.22E+00 1 1
 2.98E+04 1.05E+01 -1.29E-04 5.53E-10 -5.92E-01 2.39E+01 -2.50E-06 1.74E-10
 6.23E+02 6.64E-01 -4.19E-05 8.85E-10 1.93E+02 2.47E-02 -1.32E-06 2.36E-11
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00 0.49 0.00 0.00 0.06 0.23 0.22 0.00
 HYDRAULIC SURFACE WASH SYSTEMS SQ FT SQ FT 1.40E+02 2.80E+04 1.00E+00 1 1
 2.60E+04 2.91E+01 -1.05E-03 3.21E-08 3.41E+02 1.40E+01 -5.15E-05 2.16E-09
 2.08E+02 4.85E-02 -2.86E-06 5.82E-11 7.03E+01 6.70E-02 -5.02E-06 1.28E-10
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00 0.52 0.00 0.00 0.08 0.10 0.30 0.00
 AIR-WATER BACKWASH FACILITIES SQ FT SQ FT 1.40E+02 2.80E+04 1.00E+00 1 1
 7.04E+04 4.24E+01 -2.34E-03 5.58E-08 7.00E+00 2.42E+01 1.39E-06 6.57E-11
 6.23E+02 6.64E-01 -4.19E-05 8.85E-10 1.94E+02 2.58E-02 -1.46E-06 2.72E-11
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00 0.41 0.00 0.00 0.09 0.39 0.11 0.00
 WASH WATER SURGE BASINS GAL GAL 1.00E+04 5.00E+05 1.00E+00 1 1
 1.88E+04 3.33E+00 -1.04E-05 1.11E-11 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.01 0.00 0.30 0.18 0.44 0.05 0.00 0.02
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00 0.01 0.00 0.00 0.00 0.00 0.00 0.00
 FILTER MOD-RAP SAND TO HIGH RATES SQ FT SQ FT 1.40E+02 2.80E+04 1.00E+00 1 1
 2.05E+04 3.28E+01 -1.41E-03 3.21E-08 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00 0.00 0.00 0.00 0.38 0.45 0.17 0.00
 CONTINUOUS AUTO. BACKWASH FILTERS SQ FT 3.60E+02 7.04E+04 1.00E+00 1 1
 1.54E+05 1.76E+02 1.77E-03 -1.75E-08 7.32E+02 8.33E+00 1.80E-04 -1.79E-09
 5.09E+02 5.35E-01 1.62E-06 -2.49E-11 7.00E+02 6.51E-02 8.76E-06 -8.79E-11
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 5.67E+04 1.53E+02 3.50E-03 -3.29E-08 0.01 0.50 0.07 0.03 0.15 0.03 0.02 0.19
 RECARBONATION BASIN CU FT CU FT 7.70E+02 3.52E+04 1.00E+00 1 3
 5.42E+03 3.95E+00 -1.28E-04 2.41E-09 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00 0.07 0.00 0.20 0.32 0.39 0.02 0.00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00
 RECARBONATION-LIQUID CO2 FEED LB/DAY/LB/DAY 3.80E+02 1.50E+04 1.00E+00 1 101
 3.96E+04 2.01E+01 -1.41E-03 7.69E-08 -7.14E+01 1.90E+01 -3.18E-04 1.53E-08
 2.48E+03 1.19E+00 -9.17E-05 3.06E-09 7.14E+01 2.52E-02 -1.45E-06 4.43E-11
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 9.83E+03 1.34E+00 -1.22E-04 5.38E-09 0.00 0.59 0.00 0.00 0.21 0.09 0.00 0.11

CRV.DAT FILE (CONTINUED)

RECARB-CO2 FROM SUBMERGED BURNERLB/DAYLB/DAY 5.00E+02 1.00E+04 1.00E+00 1 3
 5.05E+04 6.33E+00 1.58E-04 -2.34E-08 1.71E+04 7.14E+01 -8.45E-03 4.76E-07
 1.36E+03 4.31E-01 -6.59E-05 3.57E-09 8.00E+01 -6.73E-09 4.09E-12 6.88E-16
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 8.65E+03 3.14E+03 5.61E-03 -4.81E-07
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00 0.56 0.00 0.00 0.20 0.17 0.07 0.00
 RECARBONATION-CO2 FROM STACK GASLR/DAYLB/DAY 2.50E+03 5.00E+04 1.00E+00 1 1
 8.84E+03 1.13E+01 -3.89E-04 4.68E-09 -1.05E+02 1.74E+01 -5.38E-06 8.69E-11
 1.28E+03 3.09E-01 -7.47E-06 7.90E-11 3.17E+01 2.88E-02 -6.18E-07 6.60E-12
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00 0.42 0.00 0.00 0.27 0.15 0.16 0.00
 MULTIPLE HEARTH RECALCINATION SQ FT SQ FT 1.79E+02 2.93E+03 1.00E+00 1 3
 4.89E+05 2.27E+03 -8.47E-01 1.28E-04 1.75E+05 9.27E+02 -4.21E-01 1.35E-04
 3.26E+03 1.67E+01 -4.01E-03 8.45E-07 1.10E+03 1.13E+01 -3.23E-03 5.39E-07
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 1.76E+07 4.88E+04 2.44E+01 -2.17E-03
 1.78E+03 3.08E+01 -1.45E-02 2.47E-06 0.00 0.63 0.00 0.00 0.27 0.01 0.01 0.08
 CONTACT BASIN-DIRECT FILTRATION CU FT CU FT 2.64E+03 5.28E+04 1.00E+00 1 3
 1.06E+04 3.83E+00 -7.18E-05 7.16E-10 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.07 0.00 0.20 0.34 0.39 0.00 0.00 0.00
 PRESSURE DIATOMITE FILTERS MGD MGD 1.00E+00 2.00E+02 1.00E+00 1 302
 2.03E+05 7.27E+04 1.09E+02 -4.53E-01 -1.43E+03 1.27E+05 -2.42E+02 9.40E-01
 1.10E+03 3.91E+02 -6.72E-01 1.58E-03 2.39E+03 6.09E+02 -5.47E+00 1.64E-02
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 1.42E+05 1.66E+04 -1.84E+01 6.76E-02 0.01 0.62 0.01 0.01 0.15 0.04 0.07 0.09
 VACUUM DIATOMITE FILTERS MGD MGD 1.00E+00 2.00E+02 1.00E+00 1 302
 4.83E+04 1.01E+05 -5.06E+01 2.09E-01 7.54E+03 5.64E+04 1.80E+01 -6.34E-02
 2.95E+02 4.49E+02 -5.04E-01 2.96E-07 2.39E+03 6.09E+02 -5.47E+00 1.64E-02
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 1.52E+04 6.17E+04 -1.06E+02 3.75E-01 0.01 0.32 0.01 0.01 0.22 0.22 0.05 0.16
 PRESSURE FILTRATION PLANTS SQ FT SQ FT 1.40E+02 2.80E+04 1.00E+00 1 1
 2.23E+05 2.01E+02 2.57E-02 -6.69E-07 2.90E+03 2.34E+02 2.36E-04 -5.36E-09
 5.17E+02 4.94E+00 -1.89E-04 4.09E-09 1.25E+03 1.37E+00 -6.16E-05 1.32E-09
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 2.01E+05 2.11E+01 9.00E-03 -2.26E-07 0.01 0.45 0.01 0.01 0.07 0.25 0.12 0.08
 IN-PLANT PUMPING MGD MGD 1.00E+00 2.00E+02 1.00E+00 1 5
 2.23E+04 5.47E+03 -1.53E+01 6.48E-02 1.41E+02 5.24E+04 1.64E+00 -4.59E-03
 2.13E+02 1.32E+02 4.54E-01 -2.49E-03 5.09E+02 2.20E+01 -1.90E-02 1.24E-04
 3.50E+01 7.50E+01 5.68E-08 4.00E-10 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 2.23E+04 5.47E+03 -1.53E+01 6.48E-02 0.01 0.22 0.02 0.03 0.28 0.27 0.11 0.06
 WASH WATER STORAGE TANKS GAL GAL 2.10E+04 9.00E+05 1.00E+00 1 1
 2.12E+03 3.89E-01 -3.82E-07 2.98E-13 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.02 0.00 0.01 0.43 0.54 0.00 0.00 0.00
 REVERSE OSMOSIS MGD MGD 1.00E+00 2.00E+02 1.00E+00 1 302
 2.46E+05 5.32E+05 -1.50E+03 4.28E+00 2.24E+05 2.19E+06 3.69E+02 -1.27E+00
 2.26E+04 6.85E+04 -7.22E+01 2.46E-01 1.81E+03 9.13E+01 -6.70E-01 2.30E-03
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 2.17E+04 8.33E+04 -1.09E+02 3.49E-01 0.00 0.61 0.00 0.00 0.12 0.00 0.15 0.12
 PRESSURE ION EXCHANGE-SOFTENING MGD MGD 1.10E+00 1.23E+02 1.00E+00 490 1101
 4.95E+04 8.59E+04 2.76E+02 -2.03E+00 -1.15E+00 2.06E+03 -7.18E-02 5.50E-04
 2.38E+02 4.33E+03 1.26E-02 -3.83E-03 2.11E+03 1.28E+02 -8.58E-01 4.75E-03
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 2.59E+04 2.78E+04 1.88E+02 -1.63E+00 0.01 0.52 0.01 0.01 0.01 0.16 0.16 0.12
 GRAVITY ION EXCHANGE-SOFTENING MGD MGD 1.50E+00 1.50E+02 1.00E+00 490 1101
 1.17E+05 6.81E+04 -2.15E+02 7.80E-01 -1.53E+00 9.81E+02 4.15E-02 -3.23E-04
 1.08E+03 3.93E+03 -2.31E+00 8.75E-03 2.11E+03 1.08E+02 -1.96E-01 1.07E-03
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 1.69E+04 1.82E+04 -4.30E+01 1.16E-01 0.01 0.59 0.04 0.03 0.09 0.10 0.06 0.08
 PRESSURE ION EXCHANG-N03 REMOVAL MGD MGD 1.10E+00 1.23E+01 1.00E+00 121 2101
 2.04E+05 2.28E+04 3.35E+04 -1.72E+03 -8.31E-01 1.73E+03 -2.09E+00 1.28E-01
 2.43E+03 2.08E+04 5.64E+02 -3.15E+01 2.04E+03 1.05E+02 1.00E+01 -7.74E-01
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 2.48E+04 2.82E+04 1.70E+02 -4.61E+01 0.01 0.68 0.01 0.01 0.11 0.06 0.06 0.06
 ACTIV. ALUMINA-FLUORIDE REMOVAL MGD MGD 7.00E-01 1.35E+02 1.00E+00 1 202
 4.46E+04 5.97E+04 1.94E+02 -1.05E+00 9.29E+00 6.22E-01 -7.15E-03 4.36E-05
 6.16E+02 1.60E+03 1.98E+01 -1.14E-01 2.41E+03 6.26E+01 7.21E-01 -2.60E-03
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 3.35E+03 2.09E+04 -8.13E-01 -2.39E-01 0.00 0.52 0.00 0.00 0.12 0.16 0.05 0.15
 GRAVITY GAC CONTACTORS-CONCRETE CU FT SQ FT 3.50E+02 1.06E+04 1.40E+02 28 3004
 6.47E+04 5.83E+01 -6.53E-03 2.96E-07 9.41E+00 4.86E+00 1.20E-06 -2.55E-11
 4.31E+02 2.78E+00 -1.37E-04 3.03E-09 8.46E+02 8.04E-01 -3.28E-05 9.39E-10
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 1.72E+04 1.93E+02 -4.11E-03 8.71E-08 0.01 0.14 0.05 0.03 0.20 0.41 0.02 0.14
 1.41E+04 2.68E+01 -3.93E-04 7.46E-09 -8.24E+01 3.86E-01 -2.13E-08 2.85E-14
 5.46E+02 1.61E-01 -3.12E-07 3.21E-13 2.32E+03 1.89E-02 9.37E-08 -9.64E-14
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 -4.52E+03 2.17E+01 -1.22E-05 1.26E-11 0.01 0.43 0.01 0.01 0.08 0.19 0.06 0.21
 PRESSURE CARBON CONTACTORS CU FT SQ FT 3.90E+02 2.26E+03 1.57E+02 679 1004
 3.94E+04 7.63E+01 -2.69E-02 4.52E-06 1.21E+02 5.00E+00 2.12E-04 -1.41E-08
 9.25E+02 4.10E+00 1.60E-04 2.88E-09 8.90E+02 7.30E-01 3.52E-05 -3.07E-09
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 4.59E+04 3.97E+02 -6.00E-02 6.91E-06 0.01 0.47 0.01 0.01 0.06 0.17 0.10 0.17

CRV.DAT FILE (CONTINUED)

CONVERT FILTER TO GAC CONTACTOR SQ FT SQ FT 3.70E+02 7.00E+04 1.00E+00 1 1
 2.03E+04 5.10E+01 -2.52E-04 1.97E-09 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 GRANULAR ACT CARBON-CONSTR COST LB LB 1.00E+04 1.00E+07 1.00E+00 1 1
 1.02E+03 6.07E-01 -6.54E-09 -5.61E-17 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 MAKEUP CARBON COST-D&M ONLY LB/YR LB/YR 1.00E+04 1.00E+07 1.00E+00 1 1
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 1.02E+03 6.07E-01 -6.54E-09 -5.61E-17 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 CAPPING SAND FILTER W/ANTHRAZITESQ FT SQ FT 3.50E+02 7.00E+04 1.00E+00 1 1
 4.08E+02 6.17E+00 -9.55E-06 9.53E-11 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 REGIONAL GAC REGEN-TRANS & STOR CU FT LB/YR 1.00E+03 2.00E+04 3.00E+04 3 6006
 1.83E+04 7.21E+00 1.87E-03 -6.84E-08 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 2.46E-03 1.99E-05 1.35E-13 -1.14E-21 -1.16E-02 2.30E-05 7.07E-14 4.37E-21
 -9.54E-03 1.93E-05 4.08E-14 2.60E-21 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 REGIONAL MULTI HEARTH GAC REGEN SQ FT SQ FT 2.70E+01 1.51E+03 1.00E+00 1 12
 4.68E+05 3.74E+03 -2.71E+00 8.31E-04 2.49E+05 1.26E+03 -8.58E-01 3.22E-04
 2.48E+03 2.78E+01 -2.95E-02 1.13E-05 2.51E+02 2.19E+01 -1.46E-02 4.94E-06
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 1.69E+06 1.59E+05 -4.87E+01 2.29E-02
 1.39E+04 2.17E+01 1.89E-02 -1.25E-05 0.00 0.53 0.00 0.00 0.28 0.02 0.01 0.16
 MULTIPLE HEARTH GAC REGENERATIONSFT SQ FT 2.70E+01 1.51E+03 1.00E+00 1 3
 4.68E+05 3.74E+03 -2.71E+00 8.31E-04 2.49E+05 1.26E+03 -8.58E-01 3.22E-04
 2.48E+03 2.78E+01 -2.95E-02 1.13E-05 2.51E+02 2.19E+01 -1.46E-02 4.94E-06
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 1.69E+06 1.59E+05 -4.87E+01 2.29E-02
 1.39E+04 2.17E+01 1.89E-02 -1.25E-05 0.00 0.53 0.00 0.00 0.28 0.02 0.01 0.16
 INFRARED CARB REGEN FURNACE LB/DAYLB/DAY 2.40E+03 6.00E+04 1.00E+00 1 1
 2.19E+05 3.15E+01 -3.64E-04 4.03E-09 -6.19E+04 3.28E+02 -4.27E-03 6.50E-08
 6.06E+03 1.24E+00 -2.46E-05 1.95E-10 2.03E+03 1.14E-01 2.17E-06 -2.35E-11
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 -3.49E+00 3.31E+00 -7.03E-05 6.95E-10 0.00 0.64 0.00 0.00 0.18 0.01 0.08 0.09
 FLUIDIZED BED GAC REGENERATION LB/DAYLB/DAY 6.00E+03 2.40E+04 1.00E+00 1 3
 7.74E+05 3.19E+01 -5.94E-04 5.97E-09 -4.60E+00 2.10E+01 -1.98E-08 1.43E-12
 1.09E+04 8.46E-01 -3.46E-05 6.28E-10 2.39E+03 -5.59E-02 7.67E-06 -1.65E-10
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 -1.64E+05 1.14E+03 -4.05E-03 9.73E-08
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00 0.00 0.35 0.00 0.15 0.01
 POWDERED CARB REGEN-FLUIDIZED BDLB/DAYLB/DAY 2.09E+02 3.34E+04 1.00E+00 1 1
 5.74E+05 3.28E+02 -1.56E-02 3.01E-07 -1.89E+03 4.52E+02 -1.91E-02 3.84E-07
 2.59E+03 2.35E-01 -7.94E-06 1.44E-10 1.20E+03 2.82E-02 5.15E-06 -1.12E-10
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 1.89E+05 3.49E+03 -4.93E-02 9.28E-07
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00 0.00 0.35 0.00 0.15 0.01
 POWDERED CARB REGEN-ATOMIZED SUSLB/DAYLB/DAY 1.00E+03 1.00E+04 1.00E+00 1 1
 1.04E+05 2.29E+02 -4.87E-03 2.13E-07 2.03E+04 2.23E+01 4.30E-03 -2.28E-07
 1.93E+03 4.43E-02 2.41E-05 -1.69E-09 9.04E+02 1.28E-01 -1.23E-05 5.60E-10
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 -2.98E+05 6.42E+03 -1.21E-01 3.27E-06
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00 0.00 0.00 0.00 0.00 0.12 0.12
 CHEM SLUDGE PUMPING-UNTHICKENED GPM GPM 2.00E+01 1.00E+04 1.00E+00 1 1
 3.28E+04 6.07E+01 -9.22E-03 5.49E-07 2.36E+00 6.39E+01 3.07E-05 -2.00E-09
 2.27E+03 7.39E+00 -9.64E-04 6.00E-08 1.07E+02 3.08E-01 -5.16E-05 2.91E-09
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 9.71E+03 3.26E+00 -5.88E-04 3.75E-08 0.01 0.15 0.06 0.06 0.24 0.23 0.14 0.11
 CHEM SLUDGE PUMPING-THICKENED GPM GPM 5.00E+00 1.25E+03 1.00E+00 1 1
 8.46E+03 1.69E+02 -2.43E-01 1.17E-04 2.98E+03 4.62E+02 -2.14E-01 9.60E-05
 1.10E+03 2.21E+01 -3.06E-02 1.47E-05 4.77E+01 9.40E-01 -1.26E-03 5.90E-07
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 4.95E-03 6.05E+00 -2.38E-03 7.70E-07 0.00 0.64 0.00 0.00 0.13 0.04 0.07 0.12
 GRAVITY SLUDGE THICKENER-LIME SQ FT SQ FT 3.14E+02 1.78E+04 1.00E+00 1 3
 4.18E+04 4.06E+01 -3.99E-03 1.58E-07 2.83E+03 1.44E+00 1.11E-04 -4.34E-09
 9.36E+01 1.59E-01 1.17E-06 -1.63E-10 1.16E+02 3.59E-02 -2.69E-06 8.67E-11
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.03 0.41 0.12 0.16 0.27 0.00 0.01 0.00
 GRAV SLDG THICKENER-ALUM & FECL3SQ FT SQ FT 3.14E+02 1.78E+04 1.00E+00 1 3
 4.18E+04 4.06E+01 -3.99E-03 1.58E-07 2.76E+03 1.69E+00 -8.49E-05 4.05E-09
 9.36E+01 1.59E-01 1.17E-06 -1.63E-10 1.16E+02 3.59E-02 -2.69E-06 8.67E-11
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.03 0.41 0.12 0.16 0.27 0.00 0.01 0.00
 VACUUM FILTERS SQ FT SQ FT 9.40E+00 1.32E+03 1.00E+00 1 1
 1.62E+05 7.36E+02 -2.69E-01 1.12E-04 7.78E+04 1.50E+03 1.84E-01 -7.19E-06
 1.63E+03 1.52E+02 -1.66E-01 7.35E-05 6.12E+02 1.58E+01 -1.39E-02 5.99E-06
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 1.27E+05 3.81E+02 -5.67E-01 3.18E-04 0.00 0.46 0.00 0.00 0.16 0.02 0.02 0.34

CRV.DAT FILE (CONTINUED)

BELT FILTER PRESS	GPM	GPM	1.50E+01	4.50E+02	1.00E+00	1	1
1.20E+05	5.65E+03	1.13E+01	-1.82E-02	4.69E+04	3.40E+03	8.73E+00	-1.31E-02
5.71E+02	5.25E+01	1.23E-01	-2.09E-04	8.03E+02	1.75E+01	2.87E-02	-2.76E-05
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
9.79E+04	1.34E+03	-3.83E+00	6.90E-03	0.00	0.69	0.00	0.00
FILTER PRESS	CU FT	CU FT	4.30E+00	8.96E+02	1.00E+00	1	1
2.03E+05	5.06E+03	-1.03E+01	7.89E-03	1.66E+04	1.92E+03	-2.34E+00	1.93E-03
9.57E+02	2.88E+01	-4.96E-02	3.64E-05	7.00E+03	7.33E+00	5.26E-02	-3.01E-05
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
1.32E+05	1.92E+03	-4.14E+00	3.05E-03	0.00	0.61	0.00	0.00
DECANTER CENTRIFUGES	GPM	GPM	1.00E+01	5.00E+02	1.00E+00	1	3
1.47E+05	1.92E+03	-4.01E+00	4.02E-03	5.16E+02	1.16E+03	8.29E-01	-1.05E-03
6.39E+02	9.18E+01	-3.09E-01	3.67E-04	5.64E+02	1.72E+01	-6.16E-02	7.64E-05
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
9.86E+04	7.87E+02	-1.62E+00	1.20E-03	0.00	0.48	0.00	0.00
BASKET CENTRIFUGES	GPD	GPD	3.60E+03	7.20E+05	1.00E+00	1	1
1.75E+05	7.66E-01	6.13E-06	-6.15E-12	6.08E+04	7.85E-01	1.11E-05	-1.07E-11
1.71E+03	1.30E-02	8.22E-08	-7.34E-14	4.78E+03	4.13E-02	1.38E-07	-1.38E-13
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
7.76E+04	8.30E-01	1.17E-05	-1.15E-11	0.00	0.53	0.00	0.00
SAND DRYING BEDS	SQ FT	SQ FT	5.00E+03	4.00E+05	1.00E+00	1	1
7.45E+03	2.97E+00	5.07E-07	-6.77E-12	0.00E+00	0.00E+00	0.00E+00	0.00E+00
-7.41E+00	3.16E-02	-9.43E-09	1.83E-14	5.74E+02	2.84E-02	6.47E-08	-9.80E-14
-1.75E-04	6.00E-02	1.12E-13	-2.90E-19	0.00E+00	0.00E+00	0.00E+00	0.00E+00
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.04	0.00	0.08	0.02
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.02	0.64	0.20
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00	0.00	0.00
SLUDGE DEWATERING LAGOONS	CU FT	CF/YR	4.00E+04	8.00E+06	6.25E-01	1	1
6.79E+03	8.13E-02	-2.06E-09	-2.55E-17	0.00E+00	0.00E+00	0.00E+00	0.00E+00
4.22E+01	8.85E-04	-8.68E-11	-2.92E-20	1.80E+01	7.71E-03	-3.45E-10	-2.32E-18
7.54E+00	9.27E-03	-1.55E-10	-1.17E-18	0.00E+00	0.00E+00	0.00E+00	0.00E+00
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.51	0.00	0.04	0.01
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00	0.28	0.16	0.00
SLUDGE DISPOSAL-SANITARY SEWER	GPM	GPM	2.00E+01	1.00E+04	1.00E+00	1	11
4.94E+01	8.43E+02	-2.11E-04	2.55E-08	0.00E+00	0.00E+00	0.00E+00	0.00E+00
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00	0.00	0.00	0.00
5.00E+03	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00	0.00	0.00	0.00
LIQUID SLUDGE HAULING	MG/YR	MG/YR	1.25E+00	1.00E+02	1.00E+00	1	7
7.23E+04	2.03E+03	6.45E+01	-3.71E-01	5.65E+04	1.76E+04	-5.40E+01	4.24E-01
7.33E+00	5.94E+02	4.53E-02	-2.70E-04	-9.35E-01	2.09E+02	4.07E-02	-3.77E-04
6.53E+01	5.07E+02	4.17E-01	-3.05E-03	0.00E+00	0.00E+00	0.00E+00	0.00E+00
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00	0.00	0.00	0.00
DEWATERED SLUDGE HAULING	CY/YR	CY/YR	1.00E+03	3.00E+05	1.00E+00	1	7
4.86E+04	1.34E+00	-7.65E-06	1.98E-11	4.10E+04	4.59E+00	-1.83E-05	4.27E-11
1.21E+02	9.79E-02	1.27E-07	-3.05E-13	8.96E+01	2.93E-02	1.11E-07	-2.74E-13
1.31E+02	8.85E-02	7.88E-08	-1.95E-13	0.00E+00	0.00E+00	0.00E+00	0.00E+00
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00	0.00	0.00	0.00
RAW WATER PUMPING FACILITY	MGD	MGD	1.00E+00	2.00E+02	1.00E+00	1	5
1.92E+04	3.43E+03	-2.89E+00	8.85E-03	-5.38E-03	4.49E+04	-9.78E-05	-1.42E-07
2.17E+02	1.33E+02	2.80E-01	-1.63E-03	4.99E+02	2.37E+01	-3.57E-02	1.66E-04
3.00E+01	1.00E+02	4.89E-04	1.34E-05	0.00E+00	0.00E+00	0.00E+00	0.00E+00
1.97E+04	5.06E+03	-8.25E+00	3.51E-02	0.00	0.42	0.00	0.00
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00	0.00	0.17	0.32
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00	0.00	0.32	0.09
FINISHED WATER PUMPING FACILITY	MGD	MGD	1.50E+00	3.00E+02	1.00E+00	1	5
3.75E+04	2.82E+03	1.50E+01	-3.27E-02	8.19E-04	5.00E+04	8.10E-05	-3.33E-07
1.89E+02	1.47E+02	-1.36E-01	1.97E-04	5.06E+02	2.13E+01	5.23E-03	1.22E-05
1.00E+02	3.00E+02	-2.19E-03	4.28E-04	0.00E+00	0.00E+00	0.00E+00	0.00E+00
4.07E+04	8.88E+03	-2.05E+01	5.27E-02	0.00	0.41	0.00	0.00
CLEARWELL STORAGE-BELOW GROUND	GAL	GAL	1.00E+04	7.50E+06	1.00E+00	1	1
3.10E+04	4.22E-01	-2.78E-08	-1.39E-17	0.00E+00	0.00E+00	0.00E+00	0.00E+00
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00	0.00	0.00	0.00
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00	0.00	0.00	0.00
CLEARWELL STORAGE-GROUND LEVEL	GAL	GAL	8.50E+03	9.40E+06	1.00E+00	1	1
2.70E+04	2.07E-01	-9.72E-09	-3.95E-17	0.00E+00	0.00E+00	0.00E+00	0.00E+00
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00	0.00	0.00	0.00
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00	0.00	0.00	0.00
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.01	0.00	0.35	0.17
DIFFUSED AERATION BASIN	CU FT	CU FT	1.90E+03	3.80E+05	1.00E+00	1	1
5.43E+04	2.99E+01	-9.75E-05	1.75E-10	-6.46E+02	1.48E+02	3.14E-05	-6.90E-11
2.98E+03	1.61E-01	-5.72E-07	8.65E-13	1.30E+03	1.27E-01	-3.12E-07	6.54E-13
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00	0.00	0.00E+00	0.00E+00
1.47E+04	5.73E-01	-2.71E-06	5.08E-12	0.01	0.61	0.02	0.03
AERATION-AERATION TOWERS	CU FT	CU FT	6.80E+02	2.56E+05	1.00E+00	1	1
2.45E+04	1.36E+01	-6.96E-05	1.76E-10	-4.02E+03	1.07E+01	-7.18E-06	2.11E-11
5.48E+02	7.07E-02	2.19E-07	-4.83E-13	4.68E+01	1.03E-02	-5.01E-08	1.38E-13
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00	0.00	0.00E+00	0.00E+00
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00	0.00	0.14	0.00
ADMIN, LAB & MAINTENANCE BUILDING	MGD	MGD	1.00E+00	2.00E+02	1.00E+00	1	1
1.83E+04	6.96E+03	-5.69E+01	1.65E-01	0.00E+00	0.00E+00	0.00E+00	0.00E+00
1.80E+03	2.52E+02	-1.71E+00	4.52E-03	1.28E+03	2.68E+02	-2.42E+00	7.31E-03
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00	0.00	0.00E+00	0.00E+00
4.16E+04	1.59E+04	-1.30E+02	3.76E-01	0.00	0.00	0.00	0.00

CRV.DAT FILE (CONTINUED)

PACKAGE COMPLETE TREATMENT PLANT	GPM	4.00E+00	1.40E+03	1.00E+00	1	409					
5.70E+04	2.27E+03	-7.84E+00	1.81E-02	7.27E+01	1.30E+02	-4.88E-01	1.36E-03				
2.85E+02	3.75E+01	-2.28E-01	4.70E-04	1.25E+03	4.87E+01	-3.26E-01	7.33E-04				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
2.80E+04	1.98E+03	-4.70E+00	8.99E-03	0.01	0.44	0.01	0.09	0.02	0.18	0.25	
PACKAGE GRAVITY FILTER PLANTS	GPM	8.00E+01	1.40E+03	1.00E+00	1	409					
9.17E+04	1.84E+03	-9.25E+00	2.65E-02	-9.69E+01	1.06E+02	-1.38E-01	4.04E-04				
7.49E+02	1.01E+01	-5.35E-02	1.49E-04	2.68E+03	4.41E+00	3.56E-02	-1.06E-04				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
9.05E+04	2.20E+03	-1.68E+01	4.41E-02	0.01	0.22	0.15	0.00	0.08	0.06	0.17	0.31
PACKAGE PRESSURE FILTRATION PLNT	GPM	7.00E-01	3.50E+02	1.00E+00	1	409					
1.82E+04	5.01E+03	-1.03E+02	8.27E-01	7.09E+00	1.22E+02	8.55E-01	-1.01E-02				
4.64E+01	1.97E+01	-4.43E-01	3.58E-03	3.57E+02	5.17E+00	-6.18E-02	9.14E-04				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
2.40E+04	1.75E+03	6.24E+00	-1.64E-01	0.01	0.43	0.01	0.00	0.13	0.02	0.12	0.28
FILTER MEDIA-RAPID SAND	SQ FT	SQ FT	4.00E+00	2.80E+02	1.00E+00	1	1				
4.50E+01	4.71E+01	-1.85E-01	4.30E-04	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
FILTER MEDIA-DUAL MEDIA	SQ FT	SQ FT	4.00E+00	2.80E+02	1.00E+00	1	1				
9.56E+01	5.56E+01	-1.34E-01	3.15E-04	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
FILTER MEDIA-MIXED MEDIA	SQ FT	SQ FT	4.00E+00	2.80E+02	1.00E+00	1	1				
1.41E+02	8.11E+01	-1.54E-01	2.91E-04	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
FILTER MEDIA-MIXED,INST W/MF SUFSQ	FT	SQ FT	4.00E+00	2.80E+02	1.00E+00	1	1				
1.08E+03	8.91E+01	-2.18E-01	4.42E-04	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
PACKAGE PRESS DIATOMITE FILTERS	GPD	2.80E+04	1.00E+06	1.00E+00	1	402					
4.43E+04	8.79E-02	1.07E-07	-7.25E-14	1.58E+01	4.86E-02	1.39E-10	2.87E-15				
1.09E+02	1.66E-03	-2.33E-09	1.32E-15	6.27E+02	2.06E-03	-2.20E-09	2.41E-15				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
2.29E+04	9.16E-02	-1.05E-07	6.71E-14	0.01	0.55	0.01	0.09	0.04	0.05	0.24	
PACKAGE VACUUM DIATOMITE FILTERS	GPM	3.00E+01	7.20E+02	1.00E+00	1	402					
4.39E+04	3.15E+02	-4.98E-01	4.57E-04	6.00E+03	1.17E+02	7.13E-02	-1.70E-04				
7.10E+01	2.83E+00	-5.79E-03	4.40E-06	6.54E+02	2.45E+00	-1.36E-03	3.23E-06				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
2.26E+04	1.22E+02	-1.45E-01	1.09E-04	0.01	0.65	0.01	0.05	0.05	0.02	0.20	
PACKAGE ULTRAFILTRATION PLANTS	GPD	2.50E+03	1.00E+06	1.00E+00	1	302					
9.01E+03	9.28E-01	-8.97E-07	5.66E-13	1.15E+03	7.39E-02	-4.18E-08	2.75E-14				
3.08E+01	6.74E-02	1.90E-08	-1.47E-14	3.52E+02	6.76E-04	2.97E-10	-2.26E-16				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
1.01E+04	3.05E-01	-2.48E-07	2.24E-13	0.01	0.64	0.01	0.00	0.07	0.01	0.13	0.13
PACKAGE GRAN ACT CARBON COLUMNS	GPD	2.50E+03	5.00E+05	1.00E+00	1	1					
8.79E+03	3.50E-01	-1.09E-06	1.29E-12	-1.16E+01	5.27E-02	-9.29E-08	1.67E-13				
8.11E+01	7.40E-03	1.93E-08	-3.00E-14	9.62E+01	7.32E-04	-1.37E-09	1.12E-15				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
5.27E+03	3.54E-01	-1.09E-06	1.11E-12	0.01	0.25	0.02	0.00	0.22	0.15	0.03	0.32
POTASSIUM PERMANGANATE FEED SYSTLR/DAYLR/DAY	1.00E-01	1.00E+01	1.00E+00	1	101						
7.36E+03	9.62E-03	6.09E-04	8.27E-05	1.80E+03	-2.34E-03	1.49E-04	2.05E-05				
5.00E+01	-6.52E-05	4.10E-06	5.70E-07	1.01E+02	-1.32E-04	8.18E-06	1.16E-06				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
2.05E+03	-2.66E-03	1.65E-04	2.36E-05	0.00	0.22	0.00	0.00	0.05	0.05	0.03	0.65
POLYMER FEED SYSTEMS	LB/DAYLR/DAY	1.00E-01	1.00E+01	1.00E+00	1	110					
1.90E+04	-9.51E-03	-1.19E-03	-2.62E-05	1.73E+04	-8.79E-03	-1.07E-03	-2.58E-05				
2.40E+02	-1.23E-04	-1.51E-05	-3.20E-07	1.98E+02	-1.04E-04	-1.24E-05	-2.76E-07				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
8.21E+03	-4.17E-03	-5.61E-04	-1.32E-05	0.00	0.67	0.00	0.00	0.04	0.02	0.07	0.20
POWDERED ACT CARBON FEED SYSTEMS	SLB/LR	1.00E+00	1.00E+01	1.00E+00	1	101					
2.93E+03	4.68E+02	-5.01E+01	2.29E+00	1.95E+03	1.69E+02	-8.96E+00	9.72E-01				
3.89E+01	1.24E+01	-1.12E+00	6.91E-02	1.34E+02	7.33E+01	-7.12E+00	3.98E-01				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
DIRECT FEED GAS CHLORINATION	LB/DAYLR/DAY	1.00E-01	1.00E+02	1.00E+00	1	101					
4.31E+03	3.92E-04	1.84E-05	4.87E-08	1.63E+03	1.48E-04	6.99E-06	1.85E-08				
4.00E+01	3.62E-06	1.70E-07	4.72E-10	1.83E+02	1.64E-05	7.79E-07	2.09E-09				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
2.56E+03	2.32E-04	1.09E-05	2.93E-08	0.00	0.35	0.00	0.00	0.08	0.03	0.05	0.49
SODIUM HYPOCHLORITE SOLUTN FEED	LB/DAYLR/DAY	1.00E-01	1.00E+02	1.00E+00	1	101					
4.31E+03	3.92E-04	1.84E-05	4.87E-08	5.70E+02	5.15E-05	2.44E-06	6.37E-09				
2.00E+01	1.81E-06	8.51E-08	2.36E-10	3.65E+02	3.33E-05	1.55E-06	4.27E-09				
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00				
2.56E+03	2.32E-04	1.09E-05	2.93E-08	0.00	0.29	0.00	0.00	0.08	0.08	0.05	0.50

CRV.DAT FILE (CONTINUED)

OZONE GENERATING AND FEED LB/DAYLB/DAY 5.00E-01 1.00E+01 1.00E+00 1 1
 2.10E+04 2.55E+03 -8.76E+00 -3.49E-01 3.78E+02 4.37E+03 -7.69E+00 -3.22E+00
 1.11E+02 1.77E+01 1.49E-02 3.37E-04 3.42E+02 5.98E+01 -6.71E+00 2.81E-01
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 6.57E+03 4.02E-03 -1.14E-03 -4.66E-06 0.00 0.68 0.00 0.00 0.11 0.00 0.00 0.21
OZONE CONTACT CHAMBER GAL/GAL 8.50E+02 1.35E+04 1.00E+00 1 1
 9.27E+02 -3.12E-02 1.84E-04 -8.89E-09 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
CHLORINE DIOXIDE GENERATING/FEE/LB/DAYLB/DAY 1.00E-01 5.00E+01 1.00E+00 1 201
 9.67E+03 7.32E-04 -2.92E-05 5.93E-07 1.24E+03 9.50E-05 -3.82E-06 7.70E-08
 1.00E+02 7.72E-06 -3.08E-07 6.05E-09 3.65E+02 2.78E-05 -1.10E-06 2.22E-08
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 4.10E+03 3.18E-04 -1.24E-05 2.52E-07 0.00 0.48 0.00 0.00 0.07 0.04 0.05 0.34
ULTRAVIOLET LIGHT DISINFECTION GPM/GPM 1.00E+01 7.80E+02 1.00E+00 1 1
 3.38E+03 3.36E+01 1.58E-03 1.45E-06 2.80E+01 4.17E+01 -7.22E-03 7.24E-06
 5.91E+01 4.07E+00 3.80E-04 -3.25E-07 2.31E+01 1.69E-02 3.17E-05 -2.87E-08
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 9.65E+03 6.48E+00 -3.90E-03 2.08E-06 0.01 0.72 0.02 0.00 0.03 0.04 0.04 0.14
REVERSE OSMOSIS GPD/GPD 2.50E+03 1.00E+06 1.00E+00 1 302
 9.96E+03 1.41E+00 -1.71E-06 1.06E-12 1.68E+03 2.65E+00 -6.22E-07 3.79E-13
 8.34E+00 9.66E-02 2.54E-09 -1.84E-15 7.56E+02 3.97E-03 -6.28E-09 3.40E-15
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 7.64E+03 7.78E-02 4.61E-08 -2.63E-14 0.00 0.71 0.00 0.00 0.14 0.00 0.09 0.06
PRESSURE ION EXCHANGE-SOFTENING GPD/GPD 7.00E+04 8.60E+05 1.00E+00 49-4101
 5.39E+04 1.59E-01 -1.44E-07 8.54E-14 7.54E+00 1.87E-03 2.87E-10 -2.06E-16
 3.89E+02 4.50E-03 -7.15E-10 3.65E-16 8.08E+02 3.01E-03 -3.92E-09 2.21E-15
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 1.02E+04 4.93E-02 -3.67E-08 1.75E-14 0.01 0.32 0.02 0.03 0.10 0.15 0.26 0.11
PRESSURE ION EXCHANG-ND3 REMOVAL GPD/GPD 7.00E+04 8.30E+05 1.00E+00 121-4101
 5.29E+04 2.16E-01 -1.56E-07 1.03E-13 -1.40E+01 2.03E-03 -4.25E-10 3.07E-16
 2.85E+02 2.32E-02 -3.52E-09 2.49E-15 7.92E+02 3.29E-03 -4.69E-09 2.81E-15
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 1.00E+04 5.28E-02 -4.35E-08 2.22E-14 0.01 0.49 0.01 0.01 0.06 0.12 0.21 0.09
ACTIVATED ALUMINA FLUORIDE REMOVAL GPD/GPD 1.27E+04 9.10E+05 1.00E+00 1 202
 3.79E+04 2.46E-01 -3.71E-07 2.25E-13 8.07E-01 2.73E-05 -7.66E-11 7.95E-17
 3.89E+02 2.56E-03 -8.74E-10 2.33E-16 7.75E+02 4.41E-03 -7.96E-09 4.94E-15
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 6.90E+03 3.41E-02 -2.26E-08 1.96E-14 0.00 0.29 0.00 0.00 0.12 0.20 0.29 0.10
BONE CHAR FLUORIDE REMOVAL GPD/GPD 1.63E+04 8.00E+05 1.00E+00 952-6201
 5.37E+04 2.18E-01 -1.53E-07 7.81E-14 1.66E+01 1.66E-04 9.52E-10 -7.61E-16
 5.21E+02 5.02E-03 -3.36E-09 2.31E-15 7.47E+02 3.97E-03 -6.53E-09 4.23E-15
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 1.86E+04 4.99E-02 1.45E-07 -1.35E-13 0.00 0.33 0.00 0.00 0.13 0.15 0.21 0.18
PACKAGE RAW WATER PUMPING-TDH=50GPM GPM 2.00E+01 7.00E+02 1.00E+00 1 1
 1.04E+04 6.20E+01 -1.25E-01 1.05E-04 4.81E-01 1.16E+02 8.61E-04 -9.36E-07
 4.13E+01 4.71E-01 -1.06E-03 8.36E-07 4.83E+01 1.11E-01 -6.50E-05 7.86E-08
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.07 0.59 0.05 0.00 0.17 0.08 0.04 0.00
PACKAGE HIGH SERVICE PUMP STATION GPM/GFM 3.00E+01 1.10E+03 1.00E+00 1 1
 1.05E+04 1.32E+01 -1.68E-03 -8.47E-07 -6.08E+02 1.47E+02 1.79E-01 -1.24E-04
 2.84E+01 5.46E-02 -4.27E-05 4.00E-08 9.75E+01 1.48E-01 -1.97E-04 9.20E-08
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00 0.80 0.00 0.00 0.12 0.06 0.02 0.00
STEEL BACKWASH/CLEARWELL TANKS GAL/GAL 5.00E+02 3.00E+04 1.00E+00 1 1
 9.23E+02 1.36E+00 -4.19E-05 8.89E-10 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.01 0.00 0.04 0.89 0.06 0.00 0.00 0.00
LIQUID SLUDGE HAULING GPD/GPD 6.80E+01 4.11E+04 1.00E+00 1 7
 3.97E+04 7.39E+00 -3.13E-04 4.93E-09 4.06E+04 1.10E+01 -2.45E-04 3.41E-09
 3.96E+01 1.54E-01 5.69E-06 -1.01E-10 2.68E+01 3.53E-02 3.98E-06 -7.15E-11
 4.04E+01 1.33E-01 5.53E-06 -1.02E-10 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00
DEWATERED SLUDGE HAULING CY/YR CY/YR 1.00E+02 5.00E+04 1.00E+00 1 7
 2.84E+03 4.26E-01 -1.01E-05 8.12E-11 3.02E+04 8.54E+00 -2.40E-04 2.79E-09
 1.92E+02 5.09E-02 3.29E-06 -4.47E-11 6.40E+00 6.09E-02 -1.74E-06 2.62E-11
 7.03E+00 1.55E-01 -4.18E-06 6.20E-11 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00
SLUDGE DISPOSAL-SANITARY SEWER GPD/GPD 5.00E+01 2.50E+04 1.00E+00 1 11
 -1.69E-02 2.40E-01 -1.63E-06 5.50E-11 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 5.00E+03 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00E+00
 0.00E+00 0.00E+00 0.00E+00 0.00E+00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00

CRV.DAT FILE (CONTINUED)

SLUDGE DEWATERING LAGOONS			CU FT	CF/YR	1.50E+03	3.00E+04	5.00E-01	1	1
1.63E+03	2.48E-01	-1.12E-05	2.63E-10	0.00E+00	0.00E+00	0.00E+00	0.00E+00		
4.60E+01	5.63E-03	-4.40E-07	1.29E-11	1.49E+01	1.28E-04	1.35E-06	-5.36E-11		
1.85E+00	1.06E-02	3.90E-07	-1.74E-11	0.00E+00	0.00E+00	0.00E+00	0.00E+00		
0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.31	0.00	0.13	0.00	0.29	0.27
				0.00	0.13	0.00	0.29	0.00	0.00
SAND DRYING BEDS			SQ FT	SQ FT	2.00E+02	8.00E+02	1.00E+00	1	1
9.18E+02	5.80E+00	1.77E-04	-7.98E-07	0.00E+00	0.00E+00	0.00E+00	0.00E+00		
3.33E+00	3.33E-02	3.68E-09	6.99E-13	1.11E+02	2.40E-01	-3.73E-06	1.99E-07		
2.33E+01	3.33E-02	8.64E-09	-1.09E-11	0.00E+00	0.00E+00	0.00E+00	0.00E+00		
0.00E+00	0.00E+00	0.00E+00	0.05	0.00	0.37	0.05	0.24	0.29	0.00

TECHNICAL REPORT DATA
(Please read Instructions on the reverse before completing)

1. REPORT NO. EPA-600/2-79-162d	2.	3. RECIPIENT'S ACCESSION NO.
4. TITLE AND SUBTITLE ESTIMATING WATER TREATMENT COSTS Volume 4. Computer User's Manual for Retrieving and Updating Cost Data		5. REPORT DATE August 1979 (Issuing Date)
		6. PERFORMING ORGANIZATION CODE
7. AUTHOR(S) Thomas S. Lineck, Robert C. Gumerman, and Russell L. Culp		8. PERFORMING ORGANIZATION REPORT NO.
9. PERFORMING ORGANIZATION NAME AND ADDRESS Culp/Wesner/Culp Consulting Engineers 2232 S.E. Bristol, Suite 210 Santa Ana, California 92707		10. PROGRAM ELEMENT NO. 1CC614, SOS 1, Task 38
		11. CONTRACT/GRANT NO. 68-03-2516
12. SPONSORING AGENCY NAME AND ADDRESS Municipal Environmental Research Laboratory--Cin., OH Office of Research and Development U.S. Environmental Protection Agency Cincinnati, Ohio 45268		13. TYPE OF REPORT AND PERIOD COVERED Final
		14. SPONSORING AGENCY CODE EPA/600/14
15. SUPPLEMENTARY NOTES Project Officer: Robert M. Clark (513) 684-7488. See also EPA-600/2-78-182 (NTIS PB284274/AS); Volume 1, EPA-600/2-79-162a; Volume 2, EPA-600/2-79-162b; and Volume 3, EPA-600/2-79-162c.		
16. ABSTRACT This report discusses unit processes and combinations of unit processes that are capable of removing contaminants included in the National Interim Primary Drinking Water Regulations. Construction and operation and maintenance cost curves are presented for 99 unit processes that are considered to be especially applicable to contaminant removal. The report is divided into four volumes. Volume 1 is a summary volume. Volume 2 presents cost curves applicable to large water supply systems with treatment capacities between 1 and 200 mgd, as well as information on virus and asbestos removal. Volume 3 includes cost curves applicable to flows of 2,500 gpd to 1 mgd. And Volume 4 is a computer program user's manual for the curves included in the report. For each unit process included in this report, conceptual designs were formulated, and construction cost curves were checked for accuracy by a second consulting engineering firm, Zurheide-Herrmann, Inc., using cost-estimating techniques similar to those used by general contractors in preparing their bids. Operation and maintenance requirements were determined individually for three categories: Energy, maintenance material, and labor. Energy requirements for the building and the process are presented separately. Costs are in October 1978 dollars.		
17. KEY WORDS AND DOCUMENT ANALYSIS		
a. DESCRIPTORS Economic analysis, Environmental engineering, Operating costs, Computer programming, Water treatment, Cost indexes, Water supply, Cost estimates, Cost analysis	b. IDENTIFIERS/OPEN ENDED TERMS Energy costs, Cost curves, Safe Drinking Water Act, Interim primary standards, Unit processes, Treatment efficiency	c. COSATI Field/Group 13B
18. DISTRIBUTION STATEMENT Release to Public		19. SECURITY CLASS <i>(This Report)</i> Unclassified
		21. NO. OF PAGES 88
		20. SECURITY CLASS <i>(This page)</i> Unclassified
		22. PRICE