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American
Boiler Manufacturers
Association

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United States
Department
of Energy

Division of Power Systems
Energy Technology Branch
Washington DC 20545

EPA

U.S. Environmental Protection Agency
Office of Research and Development

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EPA-600/7-78-136b
December 1978

Field Tests of Industrial Stoker Coal-fired Boilers for Emissions Control and Efficiency Improvement - Site A (Data Supplement)

Interagency
Energy/Environment
R&D Program Report



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December 1978

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by

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**IAG/Contract Nos. IAG-D7-E681 (EPA), EF-77-C-01-2609 (DoE)
Program Element No. EHE624**

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Prepared for

**U.S. ENVIRONMENTAL PROTECTION AGENCY
Office of Research and Development
Washington, DC 20460**

**U.S. DEPARTMENT OF ENERGY
Division of Power Systems/Energy Technology Branch
Washington, DC 20545**

and

**AMERICAN BOILER MANUFACTURERS ASSOCIATION
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FOREWORD

The purpose of this Data Supplement Volume is to document data in greater detail than was practical in the Final Technical Report.¹ It is intended to provide the necessary details to other researchers who are interested in performing their own analysis. Readers are referred to the contract final report for information as to objectives, description of facility tested and coals fired, test equipment and procedures, interpretations and conclusions. The Final Technical Report also contains data summaries not found in this volume.

The data in this volume are arranged by type (i.e., Panel Board Data, Particulate Data, etc.) and within each type by test number. Data summaries where they exist are at the front of each section. The boiler tested is referred to as Boiler A; as it is the first boiler tested under the program entitled, "A Testing Program to Update Equipment Specifications and Design Criteria for Stoker Fired Boilers."

¹Gabrielson, J. E., et al., "Field Tests of Industrial Stoker Coal-Fired Boilers for Emissions Control and Efficiency Improvement - Site A", EPA-600/7-78-136a, July, 1978.

TABLE OF CONTENTS

<u>Section</u>	<u>Page</u>
FOREWORD	ii
CONVERSION FACTORS	v
1.0 PANEL BOARD DATA	
1.1 Control Room Data Sheets	2
2.0 PARTICULATE DATA	
2.1 Particulate Data Summary	50
2.2 Particulate Data Sheets	54
2.3 Particulate Lab Worksheets	82
3.0 GASEOUS DATA	
3.1 Gaseous Emission Summary	110
3.2 Gaseous Emission Data Sheets	116
3.3 SO _x Data Summary	155
3.4 SO _x Data Sheets	158
4.0 SPECIAL TESTS DATA	
4.1 Modified Smoke Spot Data Sheet	171
4.2 Particle Size Distribution - Brink	172
- SASS	178
- BAHCO	182
- Coulter	185
4.3 Corrosion Probe Data	188
5.0 FUEL AND ASH ANALYSIS	
5.1 List of Coal and Ash Samples Analyzed	194
5.2 Commercial Testing Analysis	195
5.3 Combustibles Analysis	244
5.4 Coal Sieve Analysis	247

CONVERSION FACTORS

ENGLISH AND METRIC UNITS TO SI UNITS

<u>To Convert From</u>	<u>To</u>	<u>Multiply By</u>
in	cm	2.540
in ²	cm ²	6.452
ft	m	0.3048
ft ²	m ²	0.09290
ft ³	m ³	0.02832
lb	Kg	0.4536
lb/hr	Mg/s	0.1260
lb/10 ⁶ BTU	ng/J	430
g/Mcal	ng/J	239
BTU	J	1054
BTU/lb	J/kg	0.002324
BTU/hr	W	0.2929
J/sec	W	1.000
J/hr	W	3600
BTU/ft/hr	W/m	0.9609
BTU/ft/hr	J/hr/m	3459
BTU/ft ² /hr	W/m ²	3.152
BTU/ft ² /hr	J/hr/m ²	11349
BTU/ft ³ /hr	W/m ³	10.34
BTU/ft ³ /hr	J/hr/m ³	37234
psia	Pa	6895
"H ₂ O	Pa	249.1
Rankine	Celsius	C = 5/9R-273
Fahrenheit	Celsius	C = 5/9(F-32)
Celsius	Kelvin	K = C+273
Rankine	Kelvin	K = 5/9R

COAL FUEL ONLY

ppm @ 3% O ₂ (SO ₂)	ng/J	0.851
ppm @ 3% O ₂ (SO ₃)	ng/J	1.063
ppm @ 3% O ₂ (NO)	ng/J	0.399
ppm @ 3% O ₂ (NO ₂)	ng/J	0.611
ppm @ 3% O ₂ (CO)	ng/J	0.372
ppm @ 3% O ₂ (CH ₄)	ng/J	0.213

CONVERSION FACTORS

SI UNITS TO ENGLISH AND METRIC UNITS

<u>To Convert From</u>	<u>TO</u>	<u>Multiply By</u>
cm	in	0.3937
cm ²	in ²	0.1550
m	ft	3.281
m ²	ft ²	10.764
m ³	ft ³	35.315
Kg	lb	2.205
Mg/s	lb/hr	7.937
ng/J	lb/10 ⁶ BTU	0.00233
ng/J	g/Mcal	0.00418
J	BTU	0.000948
J/kg	BTU/lb	4.303
J/hr/m	BTU/ft/hr	0.000289
J/hr/m ²	BTU/ft ² /hr	0.0000881
J/hr/m ³	BTU/ft ³ /hr	0.0000269
W	BTU/hr	3.414
W	J/hr	0.000278
W/m	BTU/ft/hr	1.041
W/m ²	BTU/ft ² /hr	0.317
W/m ³	BTU/ft ³ /hr	0.0967
Pa	psia	0.000145
Pa	"H ₂ O	0.004014
Kelvin	Fahrenheit	F = 1.8K-460
Celsius	Fahrenheit	F = 1.8C+32
Fahrenheit	Rankine	R = F+460
Kelvin	Rankine	R = 1.8K

COAL FUEL ONLY

ng/J	ppm @ 3% O ₂ (SO ₂)	1.18
ng/J	ppm @ 3% O ₂ (SO ₃)	0.941
ng/J	ppm @ 3% O ₂ (NO)	2.51
ng/J	ppm @ 3% O ₂ (NO ₂)	1.64
ng/J	ppm @ 3% O ₂ (CO)	2.69
ng/J	ppm @ 3% O ₂ (CH ₄)	4.69

SI PREFIXES

<u>Multiplication Factor</u>	<u>Prefix</u>	<u>SI Symbol</u>
10^{12}	tera	T
10^9	giga	G
10^6	mega	M
10^3	kilo	k
10^2	hecto*	h
10^1	deka*	da
10^{-1}	deci*	d
10^{-2}	centi*	c
10^{-3}	milli	m
10^{-6}	micro	μ
10^{-9}	nano	n
10^{-12}	pico	p
10^{-15}	femto	f
10^{-18}	atto	a

*Not recommended but occasionally used

**EMISSIONS UNITS CONVERSION FACTORS
FOR TYPICAL COAL FUEL (HV = 13,320 BTU/LB)**

To Obtain Multiply by	% Weight In Fuel		lbs/10 ⁶ Btu		grams/10 ⁶ Cal		PPM (Dry @ 3% O ₂)		grains/SCF - (Dry @ 12% CO ₂)	
	S	N	SO ₂	NO ₂	SO ₂	NO ₂	SOx	NOx	SO ₂	NO ₂
% Weight In Fuel	S	1	0.666	/	0.370	/	13.2x10 ⁻⁴	/	1.48	/
	N		/	0.405	/	0.225	/	5.76x10 ⁻⁴	/	.903
lbs/10 ⁶ Btu	SO ₂	1.50	1	/	(.556)	/	19.8x10 ⁻⁴	/	(2.23)	/
	NO ₂	/		2.47	/	(.556)	/	14.2x10 ⁻⁴	/	(2.23)
grams/10 ⁶ Cal	SO ₂	2.70	/	(1.8)	1	/	35.6x10 ⁻⁴	/	(4.01)	/
	NO ₂	/	4.44	(1.8)		/	25.6x10 ⁻⁴	/	(4.01)	/
PPM (Dry @ 3% O ₂)	SOx	758	505	/	281	/	1	/	1127	/
	NOx	/	1736	704	/	391		/	1566	/
grains/SCF - (Dry @ 12% CO ₂)	SO ₂	676	(.448)	/	(.249)	/	8.87x10 ⁻⁴	/	1	
	NO ₂	/	1.11	(.448)	/	(.249)	6.39x10 ⁻⁴	/		

NOTE: 1. Values in parenthesis can be used for all flue gas constituents such as oxides of carbon, oxides of nitrogen, oxides of sulfur, hydrocarbons, particulates, etc.
2. Standard reference temperature of 530°R was used.

SECTION 1.0

PANEL BOARD DATA

	<u>PAGE</u>
1.1 CONTROL ROOM DATA SHEET	2

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 1
Date: 9 Aug 77
Description: SO_x at multiclone outlet

Time of Reading	10:02	11:17	12:21		
Stm Integrator (x 3000 lb/hr)	267870	267949	268018		
Stm Flow (% of 3x10 ⁵ lb/hr)	63	65	68		
FW Flow (% of 4x10 ⁵ lb/hr)	49	51	53		
Air Flow (% relative)	55	67	58		
Stm Hdr Press (psig)	300	300	300		
Grate Temps No. 1	604	642	742		
(°F) 2	705	650	845		
3	686	673	840		
4	577	605	726		
5	627	639	766		
6	587	678	744		
Blr Out Gas Temp (°F)	598	623	608		
AH Out Gas Temp (°F)	440	459	451		
Econ Out Gas Temp (°F)	340	352	345		
Furnace Air Temp (°F)	342	347	351		
Feedwater Temp (°F)	263	268	266		
Front OF Air, Top/Bottom (in H ₂ O)	3.6/6.0	3.6/6.0	3.6/6.0		
Rear OF Air, Top/Bottom (in H ₂ O)	- / 10.2	- / 10.2	- / 10.2		
Reinj Air, Mech/AH/Blr (in H ₂ O)					
Mech Ash Reinj, Yes or No	NO	NO	NO		
Blr Master Control (0-100%)	65	60	60		
Stoker Speed Control (0-100%)	65	60	60		
Air Flow Control (0-100%)	45	53	46		
Fur Draft Control (0-100%)	24	31	25		
Feedwater Control (0-100%)	49	50	52		
Stack Opacity (0-100%)	4.2	3.7	3.0		
COMMENTS:					

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 2

Date: 10 Aug 77

Description: Effect of Excess O₂ on Gaseous Emissions

Time of Reading	14:35	14:50	15:09	15:25	16:22
Stm Integrator (x 3000 lb/hr)	269572	269587	269606	269621	269677
Stm Flow (% of 3x10 ⁵ lb/hr)	61	61	60.5	60	61
FW Flow (% of 4x10 ⁵ lb/hr)	49	49	49	49	49
Air Flow (% relative)	51	48	44	40	50.5
Stm Hdr Press (psig)	300	300	300	300	300
Grate Temps No. 1	767	769	789	777	654
(°F) 2	824	855	889	891	745
3	820	849	876	904	732
4	719	724	711	725	690
5	778	755	750	763	749
6	805	784	787	797	830
Blr Out Gas Temp (°F)	593	584	574	570	594
AH Out Gas Temp (°F)	442	437	431	428	442
Econ Out Gas Temp (°F)	337	335	332	330	336
Furnace Air Temp (°F)	352	354	355	357	354
Feedwater Temp (°F)	264	263	262	261	263
Front OF Air, Top/Bottom (in H ₂ O)					
Rear OF Air, Top/Bottom (in H ₂ O)					
Reinj Air, Mech/AH/Blr (in H ₂ O)					
Mech Ash Reinj, Yes or No	NO	NO	NO	NO	NO
Blr Master Control (0-100%)	55	55	55	55	55
Stoker Speed Control (0-100%)	54	54	54	54	54
Air Flow Control (0-100%)	42	40	36	35	42
Fur Draft Control (0-100%)	20	18	15	14	20
Feedwater Control (0-100%)	50	50	50	50	50
Stack Opacity (0-100%)	3.0	3.0	2.8	3.7	3.0
COMMENTS:					

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 2

Date:

Description: Page 2 of 2

Time of Reading	4:37	4:51			
Stm Integrator (x 3000 lb/hr)	269692	269706			
Stm Flow (% of 3×10^5 lb/hr)	62	61	61		
FW Flow (% of 4×10^5 lb/hr)	50	49	49		
Air Flow (% relative)	53	58	63		
Stm Hdr Press (psig)	300	300	300		
Grate Temps No. 1	659	643	602		
(°F) 2	667	636	580		
3	680	624	593		
4	693	638	602		
5	728	699	674		
6	798	759	734		
Blr Out Gas Temp (°F)	599	603	608		
AH Out Gas Temp (°F)	446	448	451		
Econ Out Gas Temp (°F)	339	342	345		
Furnace Air Temp (°F)	354	351	348		
Feedwater Temp (°F)	264	265	266		
Front OF Air, Top/Bottom (in H ₂ O)					
Rear OF Air, Top/Bottom (in H ₂ O)					
Reinj Air, Mech/AH/Blr (in H ₂ O)					
Mech Ash Reinj, Yes or No	NO	NO	NO		
Blr Master Control (0-100%)	55	55	55		
Stoker Speed Control (0-100%)	54	54	54		
Air Flow Control (0-100%)	43	46	50		
Fur Draft Control (0-100%)	22	24	27		
Feedwater Control (0-100%)	51	51	50		
Stack Opacity (0-100%)		3.0	3.2		
COMMENTS:					

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 3
Date: 11 Aug 77
Description: Particulates at multiclone outlet

Time of Reading	11:46	13:58	14:54		
Stm Integrator (x 3000 lb/hr)	270818	270952	271008		
Stm Flow (% of 3x10 ⁵ lb/hr)	62	61	62		
FW Flow (% of 4x10 ⁵ lb/hr)	49	49	49		
Air Flow (% relative)	50	50	50		
Stm Hdr Press (psig)	298	300	300		
Grate Temps No. 1	593	747	756		
(°F) 2	572	818	889		
3	629	860	855		
4	621	796	781		
5	710	841	838		
6	796	817	724		
Blr Out Gas Temp (°F)	592	595	597		
AH Out Gas Temp (°F)	438	441	443		
Econ Out Gas Temp (°F)	336	338	338		
Furnace Air Temp (°F)	347	352	352		
Feedwater Temp (°F)	263	265	265		
Front OF Air, Top/Bottom (in H ₂ O)	3.6/5.6	3.6/5.6			
Rear OF Air, Top/Bottom (in H ₂ O)	—/9.7	—/9.6			
Reinj Air, Mech/AH/Blr (in H ₂ O)					
Mech Ash Reinj, Yes or No	No	No			
Blr Master Control (0-100%)	56	54	55		
Stoker Speed Control (0-100%)	55	54	54		
Air Flow Control (0-100%)	42	42	42		
Fur Draft Control (0-100%)	20	20	20		
Feedwater Control (0-100%)	52	47	50		
Stack Opacity (0-100%)	3.0	2.8	2.9		
COMMENTS:					

KVB

CONTROL ROOM DATA TEST LOCATION A

Test No.: 4
Date: 17 Aug 77
Description: Particulates and Brink at multiclone outlet

Time of Reading	12:12	14:57	16:57		
Stm Integrator (x 3000 lb/hr)	278886	279050	279170		
Stm Flow (% of 3x10 ⁵ lb/hr)	62	62	63		
FW Flow (% of 4x10 ⁵ lb/hr)	52	50	53		
Air Flow (% relative)	67	67	67		
Stm Hdr Press (psig)	300	300	300		
Grate Temps No. 1	450	436	429		
(°F) 2	556	430	435		
3	669	460	446		
4	527	475	429		
5	579	558	449		
6	600	509	565		
Blr Out Gas Temp (°F)	623	625	628		
AH Out Gas Temp (°F)	459	460	462		
Econ Out Gas Temp (°F)	350	350	350		
Furnace Air Temp (°F)	348	350	351		
Feedwater Temp (°F)	270	270	270		
Front OF Air, Top/Bottom (in H ₂ O)	3.5/5.6	3.4/5.6	3.5/5.6		
Rear OF Air, Top/Bottom (in H ₂ O)	-/10.2	-/10.5	-/10.3		
Reinj Air, Mech/AH/Blr (in H ₂ O)					
Mech Ash Reinj, Yes or No	No	No	No		
Blr Master Control (0-100%)	40	46	38		
Stoker Speed Control (0-100%)	40	46	37		
Air Flow Control (0-100%)	53	53	52		
Fur Draft Control (0-100%)	28	28	30		
Feedwater Control (0-100%)	51	54	52		
Stack Opacity (0-100%)	3.0	3.0			
COMMENTS:					

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 5
Date: 18 Aug 77
Description: Particulates at multiclone outlet

Time of Reading	11:54	12:48	13:42		
Stm Integrator (x 3000 lb/hr)	280367	280432	280496		
Stm Flow (% of 3x10 ⁵ lb/hr)	75	74			
FW Flow (% of 4x10 ⁵ lb/hr)	60	59.5			
Air Flow (% relative)	71	70			
Stm Hdr Press (psig)	300	300			
Grate Temps No. 1	460	439			
(°F) 2	472	501			
3	464	496			
4	474	470			
5	523	533			
6	658	690			
Blr Out Gas Temp (°F)	632	639			
AH Out Gas Temp (°F)	474	473			
Econ Out Gas Temp (°F)	360	360			
Furnace Air Temp (°F)	351	352			
Feedwater Temp (°F)	269	269			
Front OF Air, Top/Bottom (in H ₂ O)	3.8/5.9				
Rear OF Air, Top/Bottom (in H ₂ O)	—/10.9				
Reinj Air, Mech/AH/Blr (in H ₂ O)					
Mech Ash Reinj, Yes or No	NO				
Blr Master Control (0-100%)	57	58			
Stoker Speed Control (0-100%)	57	57			
Air Flow Control (0-100%)	57	56			
Fur Draft Control (0-100%)	33	32			
Feedwater Control (0-100%)	57	56			
Stack Opacity (0-100%)	9.5	3.4			

COMMENTS:

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 6
Date: 18 Aug 77
Description: Particulates at multiclone outlet

Time of Reading	15:35	16:26	16:58		
Stm Integrator (x 3000 lb/hr)	280630	280690	280727		
Stm Flow (% of 3x10 ⁵ lb/hr)	73	73	72		
FW Flow (% of 4x10 ⁵ lb/hr)	59	59	58		
Air Flow (% relative)	78	78	78		
Stm Hdr Press (psig)	300	300	300		
Grate Temps No. 1	480	507	468		
(°F) 2	496	553	545		
3	529	574	627		
4	577	537	588		
5	673	683	722		
6	610	645	607		
Blr Out Gas Temp (°F)	655	652	655		
AH Out Gas Temp (°F)	484	482	486		
Econ Out Gas Temp (°F)	365	380	375		
Furnace Air Temp (°F)	350	349	349		
Feedwater Temp (°F)	271	271	273		
Front OF Air, Top/Bottom (in H ₂ O)	4.0/6.3	4.0/6.1	3.9/6.1		
Rear OF Air, Top/Bottom (in H ₂ O)	—/11.5	—/11.5	—/11.2		
Reinj Air, Mech/AH/Blr (in H ₂ O)					
Mech Ash Reinj, Yes or No	No	No	No		
Blr Master Control (0-100%)	62	63	60		
Stoker Speed Control (0-100%)	62	63	60		
Air Flow Control (0-100%)	65	63	65		
Fur Draft Control (0-100%)	40	40	40		
Feedwater Control (0-100%)	56	56	55		
Stack Opacity (0-100%)	21	22	16		
COMMENTS:					

KVB

CONTROL ROOM DATA TEST LOCATION A

Test No.: 7
Date: 19 Aug 77
Description: Effect of excess O₂ on gaseous emissions

Time of Reading	9:15	9:55	10:08		
Stm Integrator (x 3000 lb/hr)	281824	281869	281885		
Stm Flow (% of 3x10 ⁵ lb/hr)	70	70			
FW Flow (% of 4x10 ⁵ lb/hr)	54	55			
Air Flow (% relative)	65	62			
Stm Hdr Press (psig)	300				
Grate Temps No. 1	656	654			
(°F) 2	653	725			
3	710	748			
4	685	714			
5	662	764			
6	683	751			
Blr Out Gas Temp (°F)	617	621			
AH Out Gas Temp (°F)	456	458			
Econ Out Gas Temp (°F)	350	350			
Furnace Air Temp (°F)	341	347			
Feedwater Temp (°F)	268	267			
Front OF Air, Top/Bottom (in H ₂ O)					
Rear OF Air, Top/Bottom (in H ₂ O)					
Reinj Air, Mech/AH/Blr (in H ₂ O)					
Mech Ash Reinj, Yes or No	NO	NO			
Blr Master Control (0-100%)	51	54			
Stoker Speed Control (0-100%)	50	52			
Air Flow Control (0-100%)	52	49			
Fur Draft Control (0-100%)	28	26			
Feedwater Control (0-100%)	52	53			
Stack Opacity (0-100%)	3.3	9.8			

COMMENTS: Boiler master on automatic, O₂ swinging with load demand, gaseous data taken where ever emissions change directions (i.e. peaks and valleys)

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 8
Date: 20 Aug 77
Description: SO_x at multiclone outlet and at stack

Time of Reading	9:54	11:11	14:53	15:31	
Stm Integrator (x 3000 lb/hr)	283427	283517	283761	283794	
Stm Flow (% of 3x10 ⁵ lb/hr)	72	71	58	54	
FW Flow (% of 4x10 ⁵ lb/hr)	55	55	44	43	
Air Flow (% relative)	69.5	70	62	50	
Stm Hdr Press (psig)				300	
Grate Temps No. 1	545	642	703	716	
(°F) 2	482	570	762	824	
3	578	555	788	833	
4	526	586	654	625	
5	648	693	608	640	
6	721	788	694	666	
Blr Out Gas Temp (°F)	623	629	601	579	
AH Out Gas Temp (°F)	460	465	447	431	
Econ Out Gas Temp (°F)	350	355	350	338	
Furnace Air Temp (°F)	342	347	346	344	
Feedwater Temp (°F)	269	270	272	268	
Front OF Air, Top/Bottom (in H ₂ O)			3.8/6.0		
Rear OF Air, Top/Bottom (in H ₂ O)			—/10.9		
Reinj Air, Mech/AH/Blr (in H ₂ O)					
Mech Ash Reinj, Yes or No	NO	NO	NO	NO	
Blr Master Control (0-100%)	68	67	49	55	
Stoker Speed Control (0-100%)	67	66	50	55	
Air Flow Control (0-100%)	58	58	45	42	
Fur Draft Control (0-100%)	30	31	21	18	
Feedwater Control (0-100%)	52	50	45	46	
Stack Opacity (0-100%)	3.2	3.0	2.8	2.8	

COMMENTS: Load unexpectedly dropped at 14:30 due to problems with the plants process equipment. First two readings multiclone out, second two readings stack test

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 9
Date: 23 Aug 77
Description: SO_x, multiclone outlet

Time of Reading	15:18	16:49			
Stm Integrator (x 3000 lb/hr)	288629	288721			
Stm Flow (% of 3x10 ⁵ lb/hr)	68	66			
FW Flow (% of 4x10 ⁵ lb/hr)	55				
Air Flow (% relative)	67	59			
Stm Hdr Press (psig)	300	305			
Grate Temps No. 1	652	714			
(°F) 2	630	723			
3	675	733			
4	588	634			
5	618	644			
6	635	696			
Blr Out Gas Temp (°F)	610	597			
AH Out Gas Temp (°F)	450	441			
Econ Out Gas Temp (°F)	344	340			
Furnace Air Temp (°F)	342	350			
Feedwater Temp (°F)	265	263			
Front OF Air, Top/Bottom (in H ₂ O)					
Rear OF Air, Top/Bottom (in H ₂ O)					
Reinj Air, Mech/AH/Blr (in H ₂ O)					
Mech Ash Reinj, Yes or No	NO	NO			
Blr Master Control (0-100%)	56				
Stoker Speed Control (0-100%)	56				
Air Flow Control (0-100%)	53				
Fur Draft Control (0-100%)	26				
Feedwater Control (0-100%)	50				
Stack Opacity (0-100%)	3.0	2.9			

COMMENTS: Large load variations during test. This was also supposed to be a Fly ash resistivity test but the WAHLCO resistivity device failed to work properly

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 10
Date: 24 Aug 77
Description: Particulates at multiclone outlet

Time of Reading	10:06	11:14	12:01		
Stm Integrator (x 3000 lb/hr)	289248	289289	289318		
Stm Flow (% of 3x10 ⁵ lb/hr)	41	36			
FW Flow (% of 4x10 ⁵ lb/hr)	34	29			
Air Flow (% relative)	45	45			
Stm Hdr Press (psig)	300	300			
Grate Temps No. 1	503	456			
(°F) 2	459	467			
3	459	495			
4	652	596			
5	862	671			
6	790	702			
Blr Out Gas Temp (°F)	564	551			
AH Out Gas Temp (°F)	413	405			
Econ Out Gas Temp (°F)	325	325			
Furnace Air Temp (°F)	333	325			
Feedwater Temp (°F)	267	271			
Front OF Air, Top/Bottom (in H ₂ O)	3.3/5.3				
Rear OF Air, Top/Bottom (in H ₂ O)	—/9.5				
Reinj Air, Mech/AH/Blr (in H ₂ O)					
Mech Ash Reinj, Yes or No	No				
Blr Master Control (0-100%)	46	38			
Stoker Speed Control (0-100%)	45	37			
Air Flow Control (0-100%)	37	38			
Fur Draft Control (0-100%)	28	28			
Feedwater Control (0-100%)	46	40			
Stack Opacity (0-100%)	3.1	3.0			

COMMENTS: Clinkers Forming under 5th and 6th Feeders

KVB

CONTROL ROOM DATA TEST LOCATION A

Test No.: 11
Date: 24 Aug 77
Description: Effect of excess O₂ on gaseous emissions

Time of Reading	13:36	13:45	13:57	14:04	14:14
Stm Integrator (x 3000 lb/hr)	289382	289388	289396	289401	289408 *
Stm Flow (% of 3x10 ⁵ lb/hr)	42	43.5	43.5	43.5	43.5
FW Flow (% of 4x10 ⁵ lb/hr)	34	35	35	35	35
Air Flow (% relative)	41	45	49.5	54	59
Stm Hdr Press (psig)	300	300	300	300	300
Grate Temps No. 1	496	461	446	434	443
(°F) 2	544	547	525	490	466
3	548	562	569	539	529
4	566	600	604	554	518
5	697	690	676	627	584
6	688	681	672	598	565
Blr Out Gas Temp (°F)	556	562	569	578	583
AH Out Gas Temp (°F)	409	413	416	422	426
Econ Out Gas Temp (°F)	325	325	327	330	332.5
Furnace Air Temp (°F)	336	334	332	330	329
Feedwater Temp (°F)	268	267	268	270	271
Front OF Air, Top/Bottom (in H ₂ O)					
Rear OF Air, Top/Bottom (in H ₂ O)					
Reinj Air, Mech/AH/Blr (in H ₂ O)					
Mech Ash Reinj, Yes or No	NO	NO	NO	NO	NO
Blr Master Control (0-100%)	48	51	50	53	53
Stoker Speed Control (0-100%)	47	50	50	52	52
Air Flow Control (0-100%)	36	40	42	45	50
Fur Draft Control (0-100%)	23	27	31	33	35
Feedwater Control (0-100%)	45	45	47	46	47
Stack Opacity (0-100%)	3.1	3.2	3.2	3.5	3.6
COMMENTS: * Final integrator reading 289415 @ 14:24					

KVB

CONTROL ROOM DATA TEST LOCATION A

Test No.: 12
Date: 24 Aug 77
Description: SO_x at multiclone outlet

Time of Reading	15:05	15:54			
Stm Integrator (x 3000 lb/hr)	289444	289481			
Stm Flow (% of 3x10 ⁵ lb/hr)	44	50			
FW Flow (% of 4x10 ⁵ lb/hr)	36	41			
Air Flow (% relative)	42.8	49			
Stm Hdr Press (psig)	300	300			
Grate Temps No. 1	617	571			
(°F) 2	527	659			
3	584	650			
4	539	525			
5	510	557			
6	612	604			
Blr Out Gas Temp (°F)	560	580			
AH Out Gas Temp (°F)	413	421			
Econ Out Gas Temp (°F)	326	327			
Furnace Air Temp (°F)	337	335			
Feedwater Temp (°F)	267	265			
Front OF Air, Top/Bottom (in H ₂ O)	3.2/5.2	3.5/5.5			
Rear OF Air, Top/Bottom (in H ₂ O)	— / 9.3	— / 9.7			
Reinj Air, Mech/AH/Blr (in H ₂ O)					
Mech Ash Reinj, Yes or No	NO	NO			
Blr Master Control (0-100%)	51	61			
Stoker Speed Control (0-100%)	50	60			
Air Flow Control (0-100%)	36	42			
Fur Draft Control (0-100%)	24	28			
Feedwater Control (0-100%)	47	52			
Stack Opacity (0-100%)	3.2	3.4			
COMMENTS:					

KVB

CONTROL ROOM DATA TEST LOCATION A

Test No.: 13
Date: 25 Aug 77
Description: Attempted Fly ash resistivity test

Time of Reading	9:42	13:08			
Stm Integrator (x 3000 lb/hr)	290599	290864			
Stm Flow (% of 3x10 ⁵ lb/hr)	81				
FW Flow (% of 4x10 ⁵ lb/hr)	65				
Air Flow (% relative)	82				
Stm Hdr Press (psig)	300				
Grate Temps No. 1	622				
(°F) 2	649				
3	716				
4	739				
5	799				
6	770				
Blr Out Gas Temp (°F)	674				
AH Out Gas Temp (°F)	497				
Econ Out Gas Temp (°F)	370				
Furnace Air Temp (°F)	356				
Feedwater Temp (°F)	268				
Front OF Air, Top/Bottom (in H ₂ O)	4.0/6.5				
Rear OF Air, Top/Bottom (in H ₂ O)	—/12.0				
Reinj Air, Mech/AH/Blr (in H ₂ O)					
Mech Ash Reinj, Yes or No	No				
Blr Master Control (0-100%)	55				
Stoker Speed Control (0-100%)	53				
Air Flow Control (0-100%)	66				
Fur Draft Control (0-100%)	40				
Feedwater Control (0-100%)	54				
Stack Opacity (0-100%)	10.0				

COMMENTS: Fly ash resistivity test unsuccessful

KVB

CONTROL ROOM DATA TEST LOCATION A

Test No.: 14
Date: 26 Aug 77
Description: Particulates and Brink at multiclone outlet

Time of Reading	9:35	10:40	11:34	13:15	17:12
Stm Integrator (x 3000 lb/hr)	292408	292488	292555	292673	292945
Stm Flow (% of 3×10^5 lb/hr)	77	77	78	72	73
FW Flow (% of 4×10^5 lb/hr)	57	56	58	53	53
Air Flow (% relative)	77	77	77	73	71
Stm Hdr Press (psig)	300	300	300	300	300
Grate Temps No. 1	464	416	378	435	426
(°F) 2	400	403	401	401	487
3	427	420	397	409	448
4	425	408	397	447	434
5	479	493	538	546	548
6	524	604	591	591	610
Blr Out Gas Temp (°F)	648	642	645	640	627
AH Out Gas Temp (°F)	475	471	474	470	463
Econ Out Gas Temp (°F)	363	362	361	360	350
Furnace Air Temp (°F)	346	343	344	344	345
Feedwater Temp (°F)	268	267	266	270	265
Front OF Air, Top/Bottom (in H ₂ O)	4.2/6.7	4.1/6.6	4.2/6.6	4.0/6.3	4.0/6.0
Rear OF Air, Top/Bottom (in H ₂ O)	—/11.6	—/11.6	—/11.6	—/11.2	—/12.0
Reinj Air, Mech/AH/Blr (in H ₂ O)					
Mech Ash Reinj, Yes or No	NO	NO	NO	NO	NO
Blr Master Control (0-100%)	55	56	60	57	65
Stoker Speed Control (0-100%)	54	56	60	56	63
Air Flow Control (0-100%)	65	65	65	61	55
Fur Draft Control (0-100%)	38	38	38	37	28
Feedwater Control (0-100%)	40	50	51	49	48
Stack Opacity (0-100%)	4.0	3.4	3.3	3.1	3.0
COMMENTS: Load dropped at 11:45 due to turbine breakdown in process section of plant.					

KVB

CONTROL ROOM DATA TEST LOCATION A

Test No.: 15
Date: 27 Aug 77
Description: Particulates at multiclone outlet

Time of Reading	11:28	12:05	13:00	13:38	
Stm Integrator (x 3000 lb/hr)	294281	294325	294393	294440	
Stm Flow (% of 3x10 ⁵ lb/hr)	71	74	78	77	
FW Flow (% of 4x10 ⁵ lb/hr)	56	59	61	60	
Air Flow (% relative)	74	74	74	74	
Stm Hdr Press (psig)	300				
Grate Temps No. 1	532		469	474	
(°F) 2	542		442	476	
3	456		493	467	
4	485		447	436	
5	612		493	486	
6	669		667	708	
Blr Out Gas Temp (°F)	636		642	642	
AH Out Gas Temp (°F)	472		475	475	
Econ Out Gas Temp (°F)	361		361	361	
Furnace Air Temp (°F)	347		351	352	
Feedwater Temp (°F)	269		267	266	
Front OF Air, Top/Bottom (in H ₂ O)					
Rear OF Air, Top/Bottom (in H ₂ O)					
Reinj Air, Mech/AH/Blr (in H ₂ O)					
Mech Ash Reinj, Yes or No	NO	NO	NO	NO	
Blr Master Control (0-100%)	54		57	59	
Stoker Speed Control (0-100%)	52		56	58	
Air Flow Control (0-100%)	61		60	60	
Fur Draft Control (0-100%)	35		35	35	
Feedwater Control (0-100%)	50		52	52	
Stack Opacity (0-100%)	3.0		3.0	3.2	

COMMENTS:

KVB

CONTROL ROOM DATA TEST LOCATION A

Test No.: 16
Date: 30 Aug 77
Description: Particulates at multiclone outlet and at ESP outlet

Time of Reading	11:54	13:39	14:51	15:38	
Stm Integrator (x 3000 lb/hr)	299445	299547	299619	299666	
Stm Flow (% of 3x10 ⁵ lb/hr)	60	60	62	61	
FW Flow (% of 4x10 ⁵ lb/hr)	47	48	49	48	
Air Flow (% relative)	64	64	64	64	
Stm Hdr Press (psig)					
Grate Temps No. 1	493	460	435	475	
(°F) 2	653	467	438	451	
3	676	442	422	449	
4	574	489	414	427	
5	535	582	539	530	
6	636	512	562	578	
Blr Out Gas Temp (°F)	613	611	611	611	
AH Out Gas Temp (°F)	453	450	450	450	
Econ Out Gas Temp (°F)	347	349	349	350	
Furnace Air Temp (°F)	347	344	345	345	
Feedwater Temp (°F)	265	268	268	269	
Front OF Air, Top/Bottom (in H ₂ O)	3.7/5.9	3.7/5.9	3.6/5.9		
Rear OF Air, Top/Bottom (in H ₂ O)	—/10.2	—/10.2	—/10.2		
Reinj Air, Mech/AH/Blr (in H ₂ O)					
Mech Ash Reinj, Yes or No	NO	NO	NO	NO	
Blr Master Control (0-100%)	45	51	48	50	
Stoker Speed Control (0-100%)	44	50	46	48	
Air Flow Control (0-100%)	51	51	51	51	
Fur Draft Control (0-100%)	27	26	26	26	
Feedwater Control (0-100%)	47	53	45	51	
Stack Opacity (0-100%)	2.5	2.5	2.5	2.6	

COMMENTS:

KVB

CONTROL ROOM DATA TEST LOCATION A

Test No.: 17

Date: 31 Aug 77

Description: Particulates at ESP outlet and at the stack

Time of Reading	14:57	16:38	18:17	19:00	
Stm Integrator (x 3000 lb/hr)	301134	301229	301309	301345	
Stm Flow (% of 3x10 ⁵ lb/hr)	67	53	52	51	
FW Flow (% of 4x10 ⁵ lb/hr)	55	45	41	41	
Air Flow (% relative)	69	52	52	52	
Stm Hdr Press (psig)	300	300	300	300	
Grate Temps No. 1	502	492	400	410	
(°F) 2	608	471	414	416	
3	729	458	473	469	
4	696	512	450	414	
5	592	537	499	434	
6	525	494	462	448	
Blr Out Gas Temp (°F)	624	577	574	563	
AH Out Gas Temp (°F)	460	425	420	416	
Econ Out Gas Temp (°F)		330	330	332	
Furnace Air Temp (°F)	348	336	334	330	
Feedwater Temp (°F)	269	264	266	268	
Front OF Air, Top/Bottom (in H ₂ O)	3.8/6.0	3.5/5.5	3.5/5.5		
Rear OF Air, Top/Bottom (in H ₂ O)	—/11.5	—/10.8	—/10.9		
Reinj Air, Mech/AH/Blr (in H ₂ O)					
Mech Ash Reinj, Yes or No	NO	NO	NO	NO	
Blr Master Control (0-100%)	43	38	27	23	
Stoker Speed Control (0-100%)	41	35	22	20	
Air Flow Control (0-100%)	53	40	40	40	
Fur Draft Control (0-100%)	27	18	17	17	
Feedwater Control (0-100%)	46	42	41	38	
Stack Opacity (0-100%)	1.0	1.0	1.0		
COMMENTS:					

KVB

CONTROL ROOM DATA TEST LOCATION A

Test No.: 18
Date: 11 Sep 77
Description: SO_x at multiclone outlet and at stack

Time of Reading	11:22	12:58	16:10	17:52	
Stm Integrator (x 3000 lb/hr)	319528	319602	319749	319828	
Stm Flow (% of 3x10 ⁵ lb/hr)	48	48	48	48	
FW Flow (% of 4x10 ⁵ lb/hr)	41	40	40	42	
Air Flow (% relative)	49.5	49.5	49.5	49.5	
Stm Hdr Press (psig)	300	300	300	300	
Grate Temps No. 1	452	400	464	452	
(°F) 2	453	419	440	429	
3	450	430	397	427	
4	509	475	397	403	
5	584	542	456	431	
6	582	559	466	432	
Blr Out Gas Temp (°F)	562	564	564	566	
AH Out Gas Temp (°F)	416	417	418	419	
Econ Out Gas Temp (°F)	330	330	332	332	
Furnace Air Temp (°F)	332	332	333	334	
Feedwater Temp (°F)	261	261	261	262	
Front OF Air, Top/Bottom (in H ₂ O)	5.1/5.9		5.0/6.8		
Rear OF Air, Top/Bottom (in H ₂ O)	—/9.4		—/9.2		
Reinj Air, Mech/AH/Blr (in H ₂ O)					
Mech Ash Reinj, Yes or No	NO	NO	NO	NO	
Blr Master Control (0-100%)	37	37	37	37	
Stoker Speed Control (0-100%)	36	36	36	36	
Air Flow Control (0-100%)	40	40	40	40	
Fur Draft Control (0-100%)	19	19	18	18	
Feedwater Control (0-100%)	51	41	50	55	
Stack Opacity (0-100%)	3.3	2.7	3.1	3.2	
COMMENTS: Unit is base loaded today and very steady					

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 19
Date: 12 Sep 77
Description: Brink cascade impactor at multiclone outlet

Time of Reading	13:53	14:49			
Stm Integrator (x 3000 lb/hr)	320723	320764			
Stm Flow (% of 3x10 ⁵ lb/hr)	47	47			
FW Flow (% of 4x10 ⁵ lb/hr)	38				
Air Flow (% relative)	43.5	43.5			
Stm Hdr Press (psig)	300	300			
Grate Temps No. 1	453	486			
(°F) 2	417	410			
3	459	451			
4	415	442			
5	476	546			
6	557	562			
Blr Out Gas Temp (°F)	552	556			
AH Out Gas Temp (°F)	411	414			
Econ Out Gas Temp (°F)	326	327			
Furnace Air Temp (°F)	339	340			
Feedwater Temp (°F)	261	262			
Front OF Air, Top/Bottom (in H ₂ O)	4.9/6.8				
Rear OF Air, Top/Bottom (in H ₂ O)	—/9.0				
Reinj Air, Mech/AH/Blr (in H ₂ O)					
Mech Ash Reinj, Yes or No	NO	NO			
Blr Master Control (0-100%)	32	32			
Stoker Speed Control (0-100%)	31	31			
Air Flow Control (0-100%)	38	38			
Fur Draft Control (0-100%)	15	15			
Feedwater Control (0-100%)	45	48			
Stack Opacity (0-100%)	3.5	3.5			

COMMENTS:

KVB

CONTROL ROOM DATA TEST LOCATION A

Test No.: 20

Date: 14 Sep 77

Description: 50x at multiclone outlet, Brink at ESP outlet

Time of Reading	9:55	12:15	14:25	
Stm Integrator (x 3000 lb/hr)	322775	322875	322966	
Stm Flow (% of 3x10 ⁵ lb/hr)	45	40	45	
FW Flow (% of 4x10 ⁵ lb/hr)	33	31		
Air Flow (% relative)	33	32	32	
Stm Hdr Press (psig)	300	300	300	
Grate Temps No. 1	514	479	607	
(°F) 2	443	459	526	
3	478	472	498	
4	511	422	486	
5	632	522	618	
6	638	564	609	
Blr Out Gas Temp (°F)	530	527	537	
AH Out Gas Temp (°F)	389	385	394	
Econ Out Gas Temp (°F)	317	312	319	
Furnace Air Temp (°F)	331	328	336	
Feedwater Temp (°F)	258	259	268	
Front OF Air, Top/Bottom (in H ₂ O)	5.3/5.0	5.5/5.0	5.2/5.0	
Rear OF Air, Top/Bottom (in H ₂ O)	—/2.0	—/3.0	—/2.0	
Reinj Air, Mech/AH/Blr (in H ₂ O)				
Mech Ash Reinj, Yes or No	No	No	No	
Blr Master Control (0-100%)	24	30	33	
Stoker Speed Control (0-100%)	23	30	32	
Air Flow Control (0-100%)	28	26	30	
Fur Draft Control (0-100%)	9	9	9	
Feedwater Control (0-100%)	39	38		
Stack Opacity (0-100%)	3.0	3.0	3.0	

COMMENTS:

KVB

CONTROL ROOM DATA TEST LOCATION A

Test No.: 21
Date: 23 Sep 77
Description: Particulates at boiler outlet without Fly ash reinjection

Time of Reading	10:30	11:37	12:42		
Stm Integrator (x 3000 lb/hr)	334470	334561	334650		
Stm Flow (% of 3x10 ⁵ lb/hr)	82	84	82		
FW Flow (% of 4x10 ⁵ lb/hr)	61	62	61		
Air Flow (% relative)	92	92	92		
Stm Hdr Press (psig)					
Grate Temps No. 1	563	511	417		
(°F) 2	565	551	505		
3	584	567	521		
4	490	450	407		
5	573	617	552		
6	658	672	662		
Blr Out Gas Temp (°F)	708	706	696		
AH Out Gas Temp (°F)	505	506	503		
Econ Out Gas Temp (°F)	385	387	387		
Furnace Air Temp (°F)	353	354	351		
Feedwater Temp (°F)	274	274	276		
Front OF Air, Top/Bottom (in H ₂ O)		5.0/5.0	5.0/5.0		
Rear OF Air, Top/Bottom (in H ₂ O)		2.7/5.0	2.7/5.0		
Reinj Air, Mech/AH/Blr (in H ₂ O)		5.0/-/-	5.0/-/-		
Mech Ash Reinj, Yes or No	No	No	No		
Blr Master Control (0-100%)	63	63	60		
Stoker Speed Control (0-100%)	61	61	59		
Air Flow Control (0-100%)	80	80	80		
Fur Draft Control (0-100%)	50	50	50		
Feedwater Control (0-100%)	58	59	60		
Stack Opacity (0-100%)	7.9	25	7.6		

COMMENTS: Grate drive shut off during entire test to allow ash bed to build up. Ash bed was one inch thick.

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 22

Date: 23 Sep 77

Description: Particulates at boiler outlet with Fly ash reinjection

Time of Reading	16:00	17:07			
Stm Integrator (x 3000 lb/hr)	334905	334998			
Stm Flow (% of 3×10^5 lb/hr)	85	86			
FW Flow (% of 4×10^5 lb/hr)	62	64			
Air Flow (% relative)	93.5	94			
Stm Hdr Press (psig)					
Grate Temps No. 1	328	323			
(°F) 2	378	354			
3	421	399			
4	360	367			
5	466	449			
6	450	378			
Blr Out Gas Temp (°F)	713	710			
AH Out Gas Temp (°F)	507	508			
Econ Out Gas Temp (°F)	391	392			
Furnace Air Temp (°F)	355	357			
Feedwater Temp (°F)	273	274			
Front OF Air, Top/Bottom (in H ₂ O)	5.0/5.0	5.0/5.0			
Rear OF Air, Top/Bottom (in H ₂ O)	5.0/3.2	5.0/3.0			
Reinj Air, Mech/AH/Blr (in H ₂ O)	9.8/-/-	10.0/-/-			
Mech Ash Reinj, Yes or No	YES	YES			
Blr Master Control (0-100%)	68	68			
Stoker Speed Control (0-100%)	67	67			
Air Flow Control (0-100%)	82	82			
Fur Draft Control (0-100%)	50	50			
Feedwater Control (0-100%)	63	64			
Stack Opacity (0-100%)	25	50			

COMMENTS: Grate drive shut down during entire test to allow ash bed to build up.
Bottom ash is forming a crust with holes corresponding to the holes on the grate.

KVB

CONTROL ROOM DATA

TEST LOCATION A

Test No.: 23

Date: 24 Sep 77

Description: Particulates at boiler outlet with Fly ash reinjection

Time of Reading	12:18	12:58	13:51		
Stm Integrator (x 3000 lb/hr)	336344	336383	336435		
Stm Flow (% of 3x10 ⁵ lb/hr)	61	61	61		
FW Flow (% of 4x10 ⁵ lb/hr)	47	47	47		
Air Flow (% relative)	59.5	60	59		
Stm Hdr Press (psig)	300				
Grate Temps No. 1	697	717	692		
(°F) 2	788	785	696		
3	793	811	745		
4	814	798	684		
5	967	863	718		
6	1003	942	837		
Blr Out Gas Temp (°F)	611	611	610		
AH Out Gas Temp (°F)	447	442	446		
Econ Out Gas Temp (°F)	350	350	350		
Furnace Air Temp (°F)	349	345	348		
Feedwater Temp (°F)	265	265	265		
Front OF Air, Top/Bottom (in H ₂ O)	5.0/5.0	5.0/6.5			
Rear OF Air, Top/Bottom (in H ₂ O)	5.0/2.7	5.0/2.7			
Reinj Air, Mech/AH/Blr (in H ₂ O)	9.0/-/-	9.0/-/-			
Mech Ash Reinj, Yes or No	YES	YES	YES		
Blr Master Control (0-100%)	44	44	44		
Stoker Speed Control (0-100%)	42	42	43		
Air Flow Control (0-100%)	45	45	45		
Fur Draft Control (0-100%)	25	25	25		
Feedwater Control (0-100%)	50	50	47		
Stack Opacity (0-100%)	3.0	2.8	2.8		

COMMENTS: Bottom ash is crusty and thin. There were no clinker problems. Note high grate temperatures.

KVB

CONTROL ROOM DATA

TEST LOCATION A

Test No.: 24

Date: 24 Sep 77

Description: Particulates at boiler outlet without Fly ash reinjection

Time of Reading	15:32	16:57			
Stm Integrator (x 3000 lb/hr)	336529	336612			
Stm Flow (% of 3×10^5 lb/hr)	61	60			
FW Flow (% of 4×10^5 lb/hr)	47	46			
Air Flow (% relative)	59	61			
Stm Hdr Press (psig)					
Grate Temps No. 1	545	657			
(°F) 2	589	636			
3	552	690			
4	511	677			
5	443	637			
6	743	714			
Blr Out Gas Temp (°F)	607	606			
AH Out Gas Temp (°F)	446	443			
Econ Out Gas Temp (°F)	350	350			
Furnace Air Temp (°F)	348	341			
Feedwater Temp (°F)	262	268			
Front OF Air, Top/Bottom (in H ₂ O)	6.1/5.0	6.2/5.1			
Rear OF Air, Top/Bottom (in H ₂ O)	5.0/2.7	5.0/2.7			
Reinj Air, Mech/AH/Blr (in H ₂ O)	6.0/-/-	6.0/-/-			
Mech Ash Reinj, Yes or No	NO	NO			
Blr Master Control (0-100%)	51	51			
Stoker Speed Control (0-100%)	50	50			
Air Flow Control (0-100%)	47	47			
Fur Draft Control (0-100%)	26	26			
Feedwater Control (0-100%)	51	50			
Stack Opacity (0-100%)	3.0	3.0			

COMMENTS:

KVB

CONTROL ROOM DATA TEST LOCATION A

Test No.: 25
Date: 5 Oct 77
Description: Gaseous only, vary overfire air

Time of Reading	10:17	11:15	11:58	13:45	
Stm Integrator (x 3000 lb/hr)	341858	341930	341979	342115	
Stm Flow (% of 3x10 ⁵ lb/hr)	80	74	74		
FW Flow (% of 4x10 ⁵ lb/hr)	58	54			
Air Flow (% relative)	89	82			
Stm Hdr Press (psig)	300	300			
Grate Temps No. 1	514	521			
(°F) 2	606	623			
3	621	645			
4	519	574			
5	702	692			
6	664	666			
Blr Out Gas Temp (°F)	703	681			
AH Out Gas Temp (°F)	502	491			
Econ Out Gas Temp (°F)	387	383			
Furnace Air Temp (°F)	354	356			
Feedwater Temp (°F)	273	272			
Front OF Air, Top/Bottom (in H ₂ O)	5.4 / 5.2	9.0 / 9.0			
Rear OF Air, Top/Bottom (in H ₂ O)	4.0 / 2.3	9.0 / 9.0			
Reinj Air, Mech/AH/Blr (in H ₂ O)	6.0 / 6.7 / -	6.0 / 6.7 / -			
Mech Ash Reinj, Yes or No	NO	NO			
Blr Master Control (0-100%)	51	50			
Stoker Speed Control (0-100%)	49	47			
Air Flow Control (0-100%)	65	58			
Fur Draft Control (0-100%)	46	43			
Feedwater Control (0-100%)	45	45			
Stack Opacity (0-100%)	4.5	3.6			

COMMENTS:

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 26 A

Date: 6 Oct 77

Description: Particulates Boiler Outlet

Time of Reading	9:52	10:49	12:02		
Stm Integrator (x 3000 lb/hr)	343683	343750	343835		
Stm Flow (% of 3x10 ⁵ lb/hr)	72	72	72		
FW Flow (% of 4x10 ⁵ lb/hr)	53	52.5	53		
Air Flow (% relative)	79	79	78		
Stm Hdr Press (psig)	300	300	300		
Grate Temps No. 1	393	471	478		
(°F) 2	395	387	448		
3	443	417	484		
4	437	485	501		
5	501	498	591		
6	633	608	645		
Blr Out Gas Temp (°F)	658	664	658		
AH Out Gas Temp (°F)	482	482	481		
Econ Out Gas Temp (°F)	379	378	377		
Furnace Air Temp (°F)	349	349	350		
Feedwater Temp (°F)	272	271	270		
Front OF Air, Top/Bottom (in H ₂ O)	6.0/6.0	6.0/6.0	6.0/6.0		
Rear OF Air, Top/Bottom (in H ₂ O)	6.0/6.0	6.0/6.0	6.0/6.0		
Reinj Air, Mech/AH/Blr (in H ₂ O)	6.0/6.5/8.8	6.0/6.5/8.8	6.0/6.5/8.7		
Mech Ash Reinj, Yes or No	NO	NO	NO		
Blr Master Control (0-100%)	44	48	50		
Stoker Speed Control (0-100%)	41	46	48		
Air Flow Control (0-100%)	55	55	55		
Fur Draft Control (0-100%)	41	41	40		
Feedwater Control (0-100%)	41	42	43		
Stack Opacity (0-100%)	3.8	4.4	4.3		
COMMENTS:					

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 26 B

Date: 6 Oct 77

Description: Particulates Multiclone Outlet

Time of Reading	15:12	16:26	16:58		
Stm Integrator (x 3000 lb/hr)	344058	344148	344188		
Stm Flow (% of 3x10 ⁵ lb/hr)	74	76.5	79		
FW Flow (% of 4x10 ⁵ lb/hr)	54.5	55.5	57		
Air Flow (% relative)	80	80	80		
Stm Hdr Press (psig)	300	300	300		
Grate Temps No. 1	433	460	463		
(°F) 2	451	478	450		
3	480	487	552		
4	595	570	547		
5	592	647	627		
6	608	614	616		
Blr Out Gas Temp (°F)	663	663	663		
AH Out Gas Temp (°F)	486	486	485		
Econ Out Gas Temp (°F)	379	378	378		
Furnace Air Temp (°F)	353	354	353		
Feedwater Temp (°F)	270	268	267		
Front OF Air, Top/Bottom (in H ₂ O)	6.0/6.0	6.0/6.0			
Rear OF Air, Top/Bottom (in H ₂ O)	6.0/6.0	6.0/6.0			
Reinj Air, Mech/AH/Blr (in H ₂ O)	6.0/6.5/8.7	6.0/6.5/8.7			
Mech Ash Reinj, Yes or No	No	No			
Blr Master Control (0-100%)	59	59	63		
Stoker Speed Control (0-100%)	56	56	60		
Air Flow Control (0-100%)	57	57	57		
Fur Draft Control (0-100%)	41	42	42		
Feedwater Control (0-100%)	43	44	46		
Stack Opacity (0-100%)	5.2	4.4	11.0		

COMMENTS:

KVB

CONTROL ROOM DATA

TEST LOCATION A

Test No.: 27

Date: 8 Oct 77

Description: SASS Boiler outlet

Time of Reading	11:07	13:15	14:46		
Stm Integrator (x 3000 lb/hr)	347319	347492	347615		
Stm Flow (% of 3×10^5 lb/hr)	83	83	83		
FW Flow (% of 4×10^5 lb/hr)	61	61			
Air Flow (% relative)	92	94	94		
Stm Hdr Press (psig)	300	300	300		
Grate Temps No. 1	499	416	485		
(°F) 2	444	438	447		
3	487	485	438		
4	509	503	511		
5	638	608	485		
6	638	637	591		
Blr Out Gas Temp (°F)	688	697	693		
AH Out Gas Temp (°F)	497	507	500		
Econ Out Gas Temp (°F)	395	400	400		
Furnace Air Temp (°F)	369	360	358		
Feedwater Temp (°F)	265	266	266		
Front OF Air, Top/Bottom (in H ₂ O)	6.0/6.0	6.0/6.0			
Rear OF Air, Top/Bottom (in H ₂ O)	6.0/6.0	6.0/6.0			
Reinj Air, Mech/AH/Blr (in H ₂ O)	5.0/6.5/8.5	5.0/6.5/8.5			
Mech Ash Reinj, Yes or No	NO	NO			
Blr Master Control (0-100%)	64	64	65		
Stoker Speed Control (0-100%)	61	61	62		
Air Flow Control (0-100%)	62	70	70		
Fur Draft Control (0-100%)	48	53	53		
Feedwater Control (0-100%)	48	47	46		
Stack Opacity (0-100%)	15	7.5	5.0		

COMMENTS:

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 28

Date: 10 Oct 77

Description: Particulates boiler outlet at minimum overfire air

Time of Reading	11:36	12:20	13:10		
Stm Integrator (x 3000 lb/hr)	351203	351264	351334		
Stm Flow (% of 3x10 ⁵ lb/hr)	84	85	85		
FW Flow (% of 4x10 ⁵ lb/hr)	62	63	62		
Air Flow (% relative)	97	98	98		
Stm Hdr Press (psig)	300	300	300		
Grate Temps No. 1	389	387	458		
(°F) 2	412	363	368		
3	389	415	422		
4	441	385	387		
5	387	376	368		
6	458	447	522		
Blr Out Gas Temp (°F)	698	704	709		
AH Out Gas Temp (°F)	505	509	510		
Econ Out Gas Temp (°F)	407	407	408		
Furnace Air Temp (°F)	368	362	365		
Feedwater Temp (°F)	265	265	265		
Front OF Air, Top/Bottom (in H ₂ O)	4.0/4.0	4.0/4.0	4.0/4.0		
Rear OF Air, Top/Bottom (in H ₂ O)	4.0/4.0	4.0/4.0	4.0/4.0		
Reinj Air, Mech/AH/Blr (in H ₂ O)	8.4/7.5/9.0	8.1/7.5/9.0	8.4/7.5/8.5		
Mech Ash Reinj, Yes or No	NO	NO	NO		
Blr Master Control (0-100%)	61	60	63		
Stoker Speed Control (0-100%)	60	57	60		
Air Flow Control (0-100%)	71	69	75		
Fur Draft Control (0-100%)	54	57	57		
Feedwater Control (0-100%)	51	49	48		
Stack Opacity (0-100%)	50	24	8.5		
COMMENTS:					

KVB

CONTROL ROOM DATA

TEST LOCATION A

Test No.: 29

Date: 10 Oct 77

Description: Particulates boiler outlet at maximum overfire air

Time of Reading	14:24	15:10	15:46		
Stm Integrator (x 3000 lb/hr)	351437	351500	351553		
Stm Flow (% of 3×10^5 lb/hr)	85	86	87		
FW Flow (% of 4×10^5 lb/hr)	62	62	62		
Air Flow (% relative)	97	97	97		
Stm Hdr Press (psig)	300	300	300		
Grate Temps No. 1	451	481	477		
(°F) 2	410	430	462		
3	451	443	441		
4	396	461	468		
5	424	438	478		
6	463	481	557		
Blr Out Gas Temp (°F)	707	709	698		
AH Out Gas Temp (°F)	512	507	502		
Econ Out Gas Temp (°F)	410	410	410		
Furnace Air Temp (°F)	369	360	358		
Feedwater Temp (°F)	266	267	267		
Front OF Air, Top/Bottom (in H ₂ O)	9.0/9.0	9.0/9.1	8.8/9.0		
Rear OF Air, Top/Bottom (in H ₂ O)	9.0/9.0	9.5/9.0	9.3/9.0		
Reinj Air, Mech/AH/Blr (in H ₂ O)	7.5/7.0/7.5	7.6/7.2/7.5	6.0/7.0/7.5		
Mech Ash Reinj, Yes or No	NO	NO	NO		
Blr Master Control (0-100%)	62	67	71		
Stoker Speed Control (0-100%)	60	64	67		
Air Flow Control (0-100%)	75	75	74		
Fur Draft Control (0-100%)	56	57	59		
Feedwater Control (0-100%)	49	49	51		
Stack Opacity (0-100%)	12	4.5	4.5		
COMMENTS:					

KVB

CONTROL ROOM DATA

TEST LOCATION A

Test No.: 30

Date: 13 Oct 77

Description: Brink cascade impactor at boiler outlet

Time of Reading	13:10	13:33	14:33		
Stm Integrator (x 3000 lb/hr)	357013	357043	357123		
Stm Flow (% of 3x10 ⁵ lb/hr)	81	82	82		
FW Flow (% of 4x10 ⁵ lb/hr)	60	59	59		
Air Flow (% relative)	90	89	90		
Stm Hdr Press (psig)	300	300	300		
Grate Temps No. 1	566	580	503		
(°F) 2	575	506	568		
3	572	598	611		
4	560	517	586		
5	594	572	648		
6	661	675	694		
Blr Out Gas Temp (°F)	683	682	677		
AH Out Gas Temp (°F)	500	501	504		
Econ Out Gas Temp (°F)	492	402	402		
Furnace Air Temp (°F)	361	361	362		
Feedwater Temp (°F)	264	264	263		
Front OF Air, Top/Bottom (in H ₂ O)	8.7/8.6	8.7/8.4	8.7/8.5		
Rear OF Air, Top/Bottom (in H ₂ O)	9.1/8.8	9.1/8.9	9.1/9.0		
Reinj Air, Mech/AH/Blr (in H ₂ O)	7.3/7.0/8.0	7.2/7.1/8.2	7.4/7.0/8.0		
Mech Ash Reinj, Yes or No	NO	NO	NO		
Blr Master Control (0-100%)	58	59	58		
Stoker Speed Control (0-100%)	56	56	55		
Air Flow Control (0-100%)	65	65	65		
Fur Draft Control (0-100%)	59	49	49		
Feedwater Control (0-100%)	47	46	47		
Stack Opacity (0-100%)	3	6	3.5		
COMMENTS:					

KVB

CONTROL ROOM DATA TEST LOCATION A

Test No.: 31
Date: 14 Oct 77
Description: Gaseous only, vary overfire air

Time of Reading	11:23	11:44	11:53	11:58	13:26
Stm Integrator (x 3000 lb/hr)	358669	358688	358646	358700	358781
Stm Flow (% of 3x10 ⁵ lb/hr)	54	54	54	54	58
FW Flow (% of 4x10 ⁵ lb/hr)	41	40	39	39	43
Air Flow (% relative)	38	38	38	38	40
Stm Hdr Press (psig)	300				300
Grate Temps No. 1	613				520
(°F) 2	577				585
3	753				696
4	737				717
5	641				472
6	709				647
Blr Out Gas Temp (°F)	559	560	559	558	584
AH Out Gas Temp (°F)	411	411	412	412	427
Econ Out Gas Temp (°F)	340	335	335	335	343
Furnace Air Temp (°F)	344	345	345	346	340
Feedwater Temp (°F)	260	260	259	259	258
Front OF Air, Top/Bottom (in H ₂ O)	4.9/5.2	5.2/1.9	4.3/9.8	4.8/5.1	4.9/5.1
Rear OF Air, Top/Bottom (in H ₂ O)	5.0/5.0	6.0/5.5	4.8/5.0	5.0/5.0	5.5/5.1
Reinj Air, Mech/AH/Blr (in H ₂ O)	7.0/8.0/9.0	7.0/7.0/9.0	7.0/7.0/9.0	6.5/7.5/9.0	7.0/6.5/9.0
Mech Ash Reinj, Yes or No	NO	NO	NO	NO	NO
Blr Master Control (0-100%)	68	28	29	40	35
Stoker Speed Control (0-100%)	20	26	26	38	33
Air Flow Control (0-100%)	29	29	29	29	37
Fur Draft Control (0-100%)	11				18
Feedwater Control (0-100%)	31				34
Stack Opacity (0-100%)	3.0	3.0	2.5	14	2.5
COMMENTS:					

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 31

Date:

Description: Page 2 of 2

Time of Reading	13:35	13:43	13:52	14:09	14:21
Stm Integrator (x 3000 lb/hr)	358789	358797	358805	358820	358832
Stm Flow (% of 3x10 ⁵ lb/hr)	58	58	58	58	58
FW Flow (% of 4x10 ⁵ lb/hr)	43	43	43	43	42
Air Flow (% relative)	48	48	49	49	49
Stm Hdr Press (psig)					
Grate Temps No. 1					
(°F) 2					
3					
4					
5					
6					
Blr Out Gas Temp (°F)	583	582	582	587	587
AH Out Gas Temp (°F)	426	426	426	428	426
Econ Out Gas Temp (°F)	343	343	344	344	349
Furnace Air Temp (°F)	340	340	340	341	341
Feedwater Temp (°F)	258	259	257	258	259
Front OF Air, Top/Bottom (in H ₂ O)	2.0/5.2	10.0/5.0	5.0/5.2	5.2/5.3	4.9/5.0
Rear OF Air, Top/Bottom (in H ₂ O)	5.5/5.2	5.5/5.0	5.0/5.2	5.5/2.0	5.0/10.0
Reinj Air, Mech/AH/Blr (in H ₂ O)	7.2/7.0/9.0	6.5/7.0/9.0	6.2/6.5/9.5	7.0/7.0/9.0	7.2/7.0/7.0
Mech Ash Reinj, Yes or No	NO	NO	NO	NO	NO
Blr Master Control (0-100%)	38	38	40	38	55
Stoker Speed Control (0-100%)	35	37	37	36	54
Air Flow Control (0-100%)	37	36	37	37	37
Fur Draft Control (0-100%)					
Feedwater Control (0-100%)					
Stack Opacity (0-100%)	2.5	2.5	3.0	2.7	10
COMMENTS:					

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 32
Date: 15 Oct 77
Description: SASS Boiler outlet

Time of Reading	12:46	13:23	14:16	15:19	16:13
Stm Integrator (x 3000 lb/hr)	360621	360674	360748	360834	360906
Stm Flow (% of 3x10 ⁵ lb/hr)	88	87.5	84.5	82.0	82.0
FW Flow (% of 4x10 ⁵ lb/hr)	64	64	61	60	59
Air Flow (% relative)	100 +	100 +	88	88	88
Stm Hdr Press (psig)	300		303	302	301
Grate Temps No. 1	448	557	576	658	667
(°F) 2	470	565	650	707	673
3	528	603	693	733	693
4	493	536	628	652	652
5	545	593	650	711	690
6	595	588	597	653	634
Blr Out Gas Temp (°F)	717	718	686	692	683
AH Out Gas Temp (°F)	514	521	499	506	496
Econ Out Gas Temp (°F)	414	416	405	404	401
Furnace Air Temp (°F)	356	362	363	366	360
Feedwater Temp (°F)	264	265	264	265	263
Front OF Air, Top/Bottom (in H ₂ O)	12.0/10.5	12.0/10.0	11.5/10.0		
Rear OF Air, Top/Bottom (in H ₂ O)	13.0/11.0	13.0/10.7	12.5/10.5		
Reinj Air, Mech/AH/Blr (in H ₂ O)	5.0/6.5/7.5	5.0/6.5/7.5		5.0/6.5/7.5	
Mech Ash Reinj, Yes or No	No	No	No	No	
Blr Master Control (0-100%)	75	68	70	64	61
Stoker Speed Control (0-100%)	72	65	66	61	59
Air Flow Control (0-100%)	80	80	62	62	62
Fur Draft Control (0-100%)	65	67	50	50	48
Feedwater Control (0-100%)	50	50	49	47	46
Stack Opacity (0-100%)	30-60	10-30	4.2	3.0	3.0
COMMENTS:					

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 33

Date: 16 Oct 77

Description: Collected ash sample for sizing tests

Time of Reading	10:58	11:55	12:33		
Stm Integrator (x 3000 lb/hr)	362407	362486	362532		
Stm Flow (% of 3x10 ⁵ lb/hr)	86	84	62		
FW Flow (% of 4x10 ⁵ lb/hr)	63	62	46		
Air Flow (% relative)	95	96	98		
Stm Hdr Press (psig)	302	302	302		
Grate Temps No. 1	425	417	448		
(°F) 2	414	409	436		
3	382	454	411		
4	437	498	449		
5	546	632	591		
6	610	629	549		
Blr Out Gas Temp (°F)	695	691	671		
AH Out Gas Temp (°F)	507	507	484		
Econ Out Gas Temp (°F)	407	408	407		
Furnace Air Temp (°F)	361	362	351		
Feedwater Temp (°F)	264	264	274		
Front OF Air, Top/Bottom (in H ₂ O)	10.0/10.0	9.9/9.8	9.8/9.8		
Rear OF Air, Top/Bottom (in H ₂ O)	10.5/10.0	10.2/9.8	10.2/9.5		
Reinj Air, Mech/AH/Blr (in H ₂ O)	4.5/6.5/7.5	5.0/6.5/7.0	5.0/6.5/7.2		
Mech Ash Reinj, Yes or No	NO	NO	NO		
Blr Master Control (0-100%)	62	62	38		
Stoker Speed Control (0-100%)	59	59	35		
Air Flow Control (0-100%)	62	72	62		
Fur Draft Control (0-100%)	54	54	54		
Feedwater Control (0-100%)	49	49	38		
Stack Opacity (0-100%)	4.0	4.0	3.0		
COMMENTS:					

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 34

Date: 29 Oct 77

Description: SASS, SO_x, Particulates at Blr out and ESP out, high OF air

Time of Reading	1103	1140	1210	1255	1323
Stm Integrator (x 3000 lb/hr)	387457	387502		387601	387635
Stm Flow (% of 3x10 ⁵ lb/hr)	78	80	78	78	77
FW Flow (% of 4x10 ⁵ lb/hr)	58	60	58	58	58
Air Flow (% relative)	62	68	66	70	73
Stm Hdr Press (psig)	303	303	303	303	303
Grate Temps No. 1	369	419	491	429	454
(°F) 2	413	464	604	510	554
3	431	497	503	511	500
4	448	520	515	506	485
5	466	522	482	520	544
6	550	585	541	586	580
Blr Out Gas Temp (°F)	621	632	631	635	637
AH Out Gas Temp (°F)	459	464	465	471	472
Econ Out Gas Temp (°F)	361	375	365	370	370
Furnace Air Temp (°F)	350	351	352	351	350
Feedwater Temp (°F)	262	262	261	262	263
Front OF Air, Top/Bottom (in H ₂ O)	10.7/10.5	10.8/10.5	10.7/10.5	10.6/10.4	10.5/10.5
Rear OF Air, Top/Bottom (in H ₂ O)	10.5/10.7	10.3/10.7	10.3/10.6	10.4/10.6	10.3/10.7
Reinj Air, Mech/AH/Blr (in H ₂ O)	6.5/6.8/7.0	6.0/6.3/8.0	5.5/6.0/7.5	5.2/6.0/7.5	5.2/6.0/7.5
Mech Ash Reinj, Yes or No	NO	NO	NO	NO	NO
Blr Master Control (0-100%)	68	68	68	68	68
Stoker Speed Control (0-100%)	66	66	66	66	66
Air Flow Control (0-100%)	45	50	50	51	52
Fur Draft Control (0-100%)	26	30	29	31	32
Feedwater Control (0-100%)	49	50	50	52	50
Stack Opacity (0-100%)					
COMMENTS: Precipitator Fields A, B + D not operating. Increased air Flow @ 12:55 because grate started to clinker up.					

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 34

Date:

Description: Page 2 of 3

Time of Reading	1355	1448	1510	1557	1646
Stm Integrator (x 3000 lb/hr)		387716	387766	387832	387893
Stm Flow (% of 3x10 ⁵ lb/hr)	76	76	82	80	76
FW Flow (% of 4x10 ⁵ lb/hr)	58	56	62	61	56
Air Flow (% relative)	71	74	77	85	74
Stm Hdr Press (psig)	304	305	304	303	302
Grate Temps No. 1	461	476	497	419	413
(°F) 2	484	601	572	440	406
3	475	510	560	437	422
4	477	517	493	445	438
5	530	492	544	570	547
6	610	605	633	541	548
Blr Out Gas Temp (°F)	634	634	652	668	636
AH Out Gas Temp (°F)	471	471	483	494	468
Econ Out Gas Temp (°F)	370	370	380	385	373
Furnace Air Temp (°F)	347	345	352	352	347
Feedwater Temp (°F)	262	263	264	267	266
Front OF Air, Top/Bottom (in H ₂ O)	10.5/10.4	10.6/10.4	10.6/10.3	10.5/10.8	10.6/10.3
Rear OF Air, Top/Bottom (in H ₂ O)	10.3/10.5	10.3/10.4	10.3/10.5	10.5/10.7	10.0/10.5
Reinj Air, Mech/AH/Blr (in H ₂ O)	5.3/6.0/8.0	5.3/6.0/8.0	5.0/6.0/8.0	5.2/6.5/8.0	5.3/6.0/8.0
Mech Ash Reinj, Yes or No	NO	NO	NO	NO	NO
Blr Master Control (0-100%)	68	70	68	67	66
Stoker Speed Control (0-100%)	67	67	67	65	64
Air Flow Control (0-100%)	52	53	55	63	46
Fur Draft Control (0-100%)	32	33	37	42	29
Feedwater Control (0-100%)	50	51	53	51	51
Stack Opacity (0-100%)					
COMMENTS:					

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 34

Date:

Description: Page 3 of 3

Time of Reading	1715				
Stm Integrator (x 3000 lb/hr)	387929				
Stm Flow (% of 3×10^5 lb/hr)	76				
FW Flow (% of 4×10^5 lb/hr)	54				
Air Flow (% relative)	72				
Stm Hdr Press (psig)	303				
Grate Temps No. 1	411				
(°F) 2	457				
3	432				
4	481				
5	598				
6	563				
Blr Out Gas Temp (°F)	635				
AH Out Gas Temp (°F)	468				
Econ Out Gas Temp (°F)	370				
Furnace Air Temp (°F)	346				
Feedwater Temp (°F)	266				
Front OF Air, Top/Bottom (in H ₂ O)	10.6/10.4				
Rear OF Air, Top/Bottom (in H ₂ O)	10.3/10.5				
Reinj Air, Mech/AH/Blr (in H ₂ O)	5.3/6.1/8.0				
Mech Ash Reinj, Yes or No	No				
Blr Master Control (0-100%)	67				
Stoker Speed Control (0-100%)	65				
Air Flow Control (0-100%)	51				
Fur Draft Control (0-100%)	32				
Feedwater Control (0-100%)	49				
Stack Opacity (0-100%)					
COMMENTS:					

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 35
Date: 30 Oct 77
Description: SASS, SO_x, Particulates at Blr out & Esp out, normal operation

Time of Reading	1240	1300	1338	1400	1445
Stm Integrator (x 3000 lb/hr)	389073			389172	
Stm Flow (% of 3x10 ⁵ lb/hr)	81	76	78	76	78
FW Flow (% of 4x10 ⁵ lb/hr)	59	56	55	54	59
Air Flow (% relative)	94	92	91	91	91
Stm Hdr Press (psig)	302	301	301	301	301
Grate Temps No. 1	321	319	344	361	335
(°F) 2	337	334	351	345	354
3	331	329	328	326	328
4	332	329	331	331	331
5	337	333	334	332	338
6	340	340	333	339	350
Blr Out Gas Temp (°F)	681	675	675	672	674
AH Out Gas Temp (°F)	497	492	492	490	493
Econ Out Gas Temp (°F)	392	390	390	387	388
Furnace Air Temp (°F)	347	342	341	340	343
Feedwater Temp (°F)	270	272	272	272	269
Front OF Air, Top/Bottom (in H ₂ O)	5.8/5.2	5.8/5.3	5.8/5.2	5.8/5.1	5.8/5.2
Rear OF Air, Top/Bottom (in H ₂ O)	6.0/5.0	6.0/5.1	6.0/5.0	6.0/5.0	6.0/5.1
Reinj Air, Mech/AH/Blr (in H ₂ O)	8.0/7.0/8.8	8.0/7.0/9.0	8.2/7.0/8.5	7.8/7.0/8.5	8.0/7.0/8.5
Mech Ash Reinj, Yes or No	NO	NO	NO	NO	NO
Blr Master Control (0-100%)	40	40	42	45	46
Stoker Speed Control (0-100%)	40	38	40	43	45
Air Flow Control (0-100%)	72	72	71	72	72
Fur Draft Control (0-100%)	42	43	43	43	43
Feedwater Control (0-100%)	48	47	50	49	51
Stack Opacity (0-100%)					
COMMENTS: Precipitator Fields A, B & D not operating					

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 35
Date:
Description: Page 2 of 2

Time of Reading	1530	1557	1628	1657	1729
Stm Integrator (x 3000 lb/hr)		389320	389361	389398	389437
Stm Flow (% of 3×10^5 lb/hr)	82	81	79	78	77
FW Flow (% of 4×10^5 lb/hr)	60	59	57	57	57
Air Flow (% relative)	90	90	90	90	91
Stm Hdr Press (psig)	301	301	301	302	301
Grate Temps No. 1	342	351	326	347	358
(°F) 2	369	357	377	383	397
3	334	329	338	343	365
4	332	328	334	333	349
5	341	336	334	345	362
6	366	344	345	350	411
Blr Out Gas Temp (°F)	677	676	671	672	671
AH Out Gas Temp (°F)	490	487	491	491	490
Econ Out Gas Temp (°F)	388	387	387	386	385
Furnace Air Temp (°F)	343	340	343	343	341
Feedwater Temp (°F)	269	269	270	271	270
Front OF Air, Top/Bottom (in H ₂ O)	5.8/5.2	5.8/5.2	5.8/5.1	5.8/5.2	5.8/5.2
Rear OF Air, Top/Bottom (in H ₂ O)	6.0/5.2	6.0/5.0	6.0/5.0	6.0/5.0	6.0/5.0
Reinj Air, Mech/AH/Blr (in H ₂ O)	8.2/7.0/8.5	8.2/7.0/8.5	7.8/7.0/8.5	7.5/7.0/8.5	8.2/7.2/8.5
Mech Ash Reinj, Yes or No	NO	NO	NO	NO	NO
Blr Master Control (0-100%)	46	47	48	50	50
Stoker Speed Control (0-100%)	45	45	46	47	47
Air Flow Control (0-100%)	72	72	72	82	82
Fur Draft Control (0-100%)	43	42	42	43	42
Feedwater Control (0-100%)	52	52	55	45	45
Stack Opacity (0-100%)					
COMMENTS:					

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 36

Date: 1 Nov 77

Description: Particulates at boiler outlet without Fly ash reinjection

Time of Reading	10:05	10:49	13:02		
Stm Integrator (x 3000 lb/hr)	392241	392300	392463		
Stm Flow (% of 3x10 ⁵ lb/hr)	80	82			
FW Flow (% of 4x10 ⁵ lb/hr)	55	62			
Air Flow (% relative)	72	74			
Stm Hdr Press (psig)	300	300			
Grate Temps No. 1	349	346			
(°F) 2	344	366			
3	404	380			
4	398	399			
5	494	434			
6	580	476			
Blr Out Gas Temp (°F)	656	660			
AH Out Gas Temp (°F)	484	487			
Econ Out Gas Temp (°F)	370	375			
Furnace Air Temp (°F)	352	352			
Feedwater Temp (°F)	265	265			
Front OF Air, Top/Bottom (in H ₂ O)	5.0/5.0	5.0/5.0			
Rear OF Air, Top/Bottom (in H ₂ O)	6.5/2.7	6.5/2.8			
Reinj Air, Mech/AH/Blr (in H ₂ O)	7.0/7.0/8.5	7.0/7.0/8.8			
Mech Ash Reinj, Yes or No	NO	NO			
Blr Master Control (0-100%)	50	46			
Stoker Speed Control (0-100%)	49	45			
Air Flow Control (0-100%)	57	57			
Fur Draft Control (0-100%)	36	36			
Feedwater Control (0-100%)	50	46			
Stack Opacity (0-100%)	4.0	4.0			
COMMENTS: Control linkage on FD Fan changed Oct 29. Boiler tripped out due to low drum level, estimated 1-2 points sampled during this period.					

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 37

Date: 1 Nov 77

Description: Particulates at boiler outlet with Fly ash reinjection

Time of Reading	16:07	17:08			
Stm Integrator (x 3000 lb/hr)	392717	392805			
Stm Flow (% of 3x10 ⁵ lb/hr)	86	86			
FW Flow (% of 4x10 ⁵ lb/hr)	63	63			
Air Flow (% relative)	77	77			
Stm Hdr Press (psig)	303				
Grate Temps No. 1	357	359			
(°F) 2	421	364			
3	392	364			
4	419	416			
5	453	467			
6	446	480			
Blr Out Gas Temp (°F)	666	672			
AH Out Gas Temp (°F)	492	494			
Econ Out Gas Temp (°F)	383	385			
Furnace Air Temp (°F)	356	358			
Feedwater Temp (°F)	264	265			
Front OF Air, Top/Bottom (in H ₂ O)	5.0/5.0	5.0/5.0			
Rear OF Air, Top/Bottom (in H ₂ O)	6.0/2.8	6.0/2.8			
Reinj Air, Mech/AH/Blr (in H ₂ O)	8.0/7.0/8.5	8.3/7.0/8.5			
Mech Ash Reinj, Yes or No	YES	YES			
Blr Master Control (0-100%)	45	45			
Stoker Speed Control (0-100%)	45	44			
Air Flow Control (0-100%)	60	60			
Fur Draft Control (0-100%)	38	40			
Feedwater Control (0-100%)	52	55			
Stack Opacity (0-100%)	4.5	3.5			
COMMENTS:					

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 38
Date: 2 Nov 77
Description: Particulates at boiler outlet, maximum O.F. air

Time of Reading	11:07	11:55	12:19	12:36	
Stm Integrator (x 3000 lb/hr)	394052	394100	394122	394139	
Stm Flow (% of 3x10 ⁵ lb/hr)	62	60	60		
FW Flow (% of 4x10 ⁵ lb/hr)	46	45	45		
Air Flow (% relative)	48	50	50		
Stm Hdr Press (psig)	300	302	301		
Grate Temps No. 1	359	363	369		
(°F) 2	357	373	398		
3	364	402	378		
4	441	465	484		
5	611	606	616		
6	729	501	554		
Blr Out Gas Temp (°F)	592	586	585		
AH Out Gas Temp (°F)	440	434	432		
Econ Out Gas Temp (°F)	345	344	344		
Furnace Air Temp (°F)	348	342	341		
Feedwater Temp (°F)	262	265	262		
Front OF Air, Top/Bottom (in H ₂ O)	10.4/10.3				
Rear OF Air, Top/Bottom (in H ₂ O)	10.5/10.5				
Reinj Air, Mech/AH/Blr (in H ₂ O)	4.8/5.9/7.5				
Mech Ash Reinj, Yes or No	No				
Blr Master Control (0-100%)	30	30	30		
Stoker Speed Control (0-100%)	30	29	30		
Air Flow Control (0-100%)	39	40	40		
Fur Draft Control (0-100%)	19	20	20		
Feedwater Control (0-100%)	40	40	38		
Stack Opacity (0-100%)	3.0	2.4	2.4		

COMMENTS:

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 39

Date: 2 Nov 77

Description: Particulates at boiler outlet, minimum O.F. air

Time of Reading	15:36	16:12	16:59	17:27	
Stm Integrator (x 3000 lb/hr)	394302	394337	394379	394408	
Stm Flow (% of 3x10 ⁵ lb/hr)	62	60	60	62	
FW Flow (% of 4x10 ⁵ lb/hr)	45	45	43	48	
Air Flow (% relative)	53	52	52	51	
Stm Hdr Press (psig)	300	301	301	301	
Grate Temps No. 1	384	364	363	376	
(°F) 2	401	389	365	370	
3	458	459	391	373	
4	438	434	431	413	
5	441	445	515	523	
6	566	555	567	640	
Blr Out Gas Temp (°F)	587	588	591	599	
AH Out Gas Temp (°F)	434	431	433	436	
Econ Out Gas Temp (°F)	344	340	340	340	
Furnace Air Temp (°F)	341	334	335	337	
Feedwater Temp (°F)	261	260	261	259	
Front OF Air, Top/Bottom (in H ₂ O)	3.0/3.0	3.0/3.0	3.0/3.0	3.0/3.0	
Rear OF Air, Top/Bottom (in H ₂ O)	3.0/3.0	3.0/3.0	3.0/3.0	3.0/3.0	
Reinj Air, Mech/AH/Blr (in H ₂ O)	5.5/6.5/9.0	5.5/6.0/9.0	5.5/6.5/9.0	5.5/6.5/9.0	
Mech Ash Reinj, Yes or No	NO	NO	NO	NO	
Blr Master Control (0-100%)	31	31	31	31	
Stoker Speed Control (0-100%)	31	31	31	31	
Air Flow Control (0-100%)	41	41	40	41	
Fur Draft Control (0-100%)	17	17	17	17	
Feedwater Control (0-100%)	42	41	40	43	
Stack Opacity (0-100%)	3.0	4.0	9.0	9.0	
COMMENTS: Testing stopped between 16:35 and 17:00 when Feeder no. 4 broke down and load dropped.					

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 40
Date: 11 Nov 77
Description: SASS at boiler outlet

Time of Reading	10:32	12:05	13:30	14:16	14:56
Stm Integrator (x 3000 lb/hr)	406781	406884	406979	407029	407073
Stm Flow (% of 3x10 ⁵ lb/hr)	69	69	69	69	68
FW Flow (% of 4x10 ⁵ lb/hr)	49	49	48	49	49
Air Flow (% relative)	76	77	78	79	79
Stm Hdr Press (psig)	302	302	302	302	301
Grate Temps No. 1	315	316	335	322	316
(°F) 2	315	320	326	325	327
3	319	321	325	322	322
4	315	320	328	321	322
5	339	343	368	350	351
6	315	324	325	322	319
Blr Out Gas Temp (°F)	633	633	636	636	633
AH Out Gas Temp (°F)	465	467	470	468	468
Econ Out Gas Temp (°F)	370	370	370	372	373
Furnace Air Temp (°F)	333	336	348	347	347
Feedwater Temp (°F)	268	268	271	268	268
Front OF Air, Top/Bottom (in H ₂ O)	5.6/5.2	5.7/5.3	5.6/5.3	5.6/5.3	5.6/5.4
Rear OF Air, Top/Bottom (in H ₂ O)	5.9/5.6	5.9/5.2	5.8/5.2	5.8/5.2	5.9/5.5
Reinj Air, Mech/AH/Blr (in H ₂ O)	5.0/9.0/9.0	5.2/9.0/9.0	5.5/9.0/9.0	5.5/9.0/9.0	5.5/9.0/9.0
Mech Ash Reinj, Yes or No	NO	NO	NO	NO	NO
Blr Master Control (0-100%)	48	48	48	48	48
Stoker Speed Control (0-100%)	48	48	48	47	47
Air Flow Control (0-100%)	65	65	66	65	65
Fur Draft Control (0-100%)	35	35	36	35	35
Feedwater Control (0-100%)	49	46	46	45	46
Stack Opacity (0-100%)	4.0	3.5	3.5	3.5	3.5

COMMENTS: Sampling started at about 13:30 after a previous False start.

KVB

CONTROL ROOM DATA
TEST LOCATION A

Test No.: 40

Date:

Description: Page 2 of 2

Time of Reading	15:44	16:23	17:00	17:45	
Stm Integrator (x 3000 lb/hr)	407127	407169	407210	407258	
Stm Flow (% of 3x10 ⁵ lb/hr)	68	67	67	66	
FW Flow (% of 4x10 ⁵ lb/hr)	50	48	48	46	
Air Flow (% relative)	80	78	77	79	
Stm Hdr Press (psig)	302	302	301	301	
Grate Temps No. 1	316	325	323	315	
(°F) 2	324	320	323	327	
3	329	320	319	318	
4	321	329	324	328	
5	347	350	362	395	
6	324	324	326	334	
Blr Out Gas Temp (°F)	633	635	633	631	
AH Out Gas Temp (°F)	467	467	468	465	
Econ Out Gas Temp (°F)	370	370	371	371	
Furnace Air Temp (°F)	344	336	339	343	
Feedwater Temp (°F)	269	269	268	269	
Front OF Air, Top/Bottom (in H ₂ O)	5.8/5.4	5.7/5.4	5.7/5.4	5.7/5.4	
Rear OF Air, Top/Bottom (in H ₂ O)	5.9/5.5	5.9/5.5	5.9/5.6	5.8/5.6	
Reinj Air, Mech/AH/Blr (in H ₂ O)	5.5/8.5/9.0	5.5/8.5/9.0	5.5/9.0/9.0	5.5/9.0/9.0	
Mech Ash Reinj, Yes or No	NO	NO	NO	NO	
Blr Master Control (0-100%)	49	50	50	50	
Stoker Speed Control (0-100%)	46	49	49	49	
Air Flow Control (0-100%)	65	65	65	65	
Fur Draft Control (0-100%)	35	35	35	35	
Feedwater Control (0-100%)	42	45	46	44	
Stack Opacity (0-100%)	3.3	3.3	3.3	3.3	
COMMENTS:					

SECTION 2.0

PARTICULATE DATA

		<u>PAGE</u>
2.1	PARTICULATE DATA SUMMARY - PART I & II	50
2.2	PARTICULATE DATA SHEET	54
2.3	PARTICULATE LAB WORKSHEET	82

PARTICULATE DATA SUMMARY
PART I

LOCATION: A

TEST NO.	Total Mass mgm.	Dry Gas Volume ft ³	Liquid Coll. ml.	Baro. Press. "Hg	Static Press. "H ₂ O	Pitot ΔP "H ₂ O	Orifice ΔH "H ₂ O	Stack Gas Temp. °R	Excess O ₂ %	Sampling Time min.	Nozzle Dia. in.	Pitot Factor n.d.	Fuel Factor SCF/10 ⁶ BTU	Flue Gas MW g/g mole
3	684.2	40.590	66.4	23.59	-2.2	.1728	1.19	876	4.1	42	.377	.837	9973	29.72
4	649.2	39.194	64.0	24.03	-3.1	.213	1.203	893	6.3	42	.377	.837	9973	29.34
5	868.2	44.737	75.6	23.99	-3.1	.2238	.697	913	4.1	63	.317	.837	9973	29.63
6	1216.0	48.507	85.3	23.99	-4.2	.261	.81	917	5.8	63	.317	.837	9973	29.40
10	492.1	47.937	53.3	23.81	-2.2	.141	.759	852	9.9	63	.377	.837	9973	29.18
14	823.2	46.222	83.1	23.77	-3.7	.2633	.730	904	5.4	63	.317	.837	9973	29.33
15	716.5	43.972	72.2	23.81	-3.6	.2519	.679	914	4.5	63	.317	.837	9973	29.55
16A	518.1	39.019	66.6	23.66	-2.7	.2133	.5876	886	6.1	63	.317	.837	9818	29.29
16B	37.9	13.986	19.5	23.66	+5.5	.6933	.2375	775	7.45	30	.187	.666	9818	29.33
		82.768	115.2			1.493	1.104	776	7.45	90	.248	.666		
17A	26.4	56.782	76.7	23.77	+5.0	1.102	.2908	769	7.3	120	.188	.666	9818	29.49
17B	22.9	30.644	67.0	23.77	0.0	.2419	.3638	621	7.8	56	.248	.817	9818	28.83
		46.989	102.8			.2656	.4213	621	7.8	56	.316	.817		
21	9982.8	28.380	50.0	23.74	-.69	.1425	.6821	1121	4.5	42	.376	.837	9779	29.50
22	15760.6	31.940	60.6	23.74	-.66	.1658	.8092	1123	4.1	42	.376	.837	9779	29.45
23	5961.8	17.646	29.7	23.62	-.55	.0739	.3891	1032	4.4	34.5	.376	.837	9779	29.53
24	4719.1	19.806	34.2	23.62	-.42	.0813	.4344	1037	4.8	34.5	.381	.837	9779	29.47
26A	6393.3	23.358	52.3	23.77	-.54	.1121	.5899	1079	5.05	36	.381	.837	9779	29.09
26B	840.3	48.558	82.7	23.77	-4.4	.3052	.8157	929	4.6	63	.317	.837	9779	29.53
28	16263.9	26.413	47.0	23.78	-.74	.1663	.7958	1142	3.9	36	.382	.837	9779	29.42
29	12150.3	26.056	44.0	23.80	-.85	.1550	.7750	1145	3.8	36	.382	.837	9779	29.61

LOCATION: A

[illegible]

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PARTICULATE DATA SUMMARY
PART II

Location A

TEST NO.	LOAD %	O ₂ %	CONDITIONS	EMISSIONS			Moisture %	Stack Gas Velocity Ft/sec	Stack Gas Flow SCF/sec	Isokin. %
				lb/10 ⁶ BTU	GR/SCF	LB/HR				
3	61	4.1	Mech outlet	0.582	0.329	153	8.92	33.25	905	114
4	60	6.3	Mech outlet	0.646	0.317	164	8.76	37.34	1006	101
5	72	4.1	Mech outlet	0.660	0.373	194	9.07	38.54	1014	108
6	70	5.8	Mech outlet	0.940	0.481	271	9.40	41.95	1095	108
10	37	9.9	Mech outlet	0.537	0.199	86	6.20	29.85	837	95
14	74	5.4	Mech outlet	0.663	0.345	196	9.67	42.05	1104	102
15	73	4.5	Mech outlet	0.572	0.315	174	8.89	41.16	1071	99
16A	59	6.1	Mech outlet	0.512	0.259	134	9.27	37.52	1004	94
16B	59	6.1	ESP outlet	.0166	.0076	4.04	7.68	67.13	1032	102
17A	52	6.3	ESP outlet	.0194	.0090	4.25	7.45	62.12	915	102
17B	52	6.3	Stack	.0128	.0057	2.82	11.52	33.48	958	104
21	82	4.5	Blr outlet, without reinjection	12.124	6.815	4275	9.50	34.21	1220	100
22	83	4.1	Blr outlet, with reinjection	16.631	9.575	6719	10.16	36.96	1365	102
23	59	4.4	Blr outlet, with reinjection	11.667	6.598	3098	9.17	23.68	913	101
24	59	4.8	Blr outlet, without reinjection	8.431	4.652	2288	9.38	24.92	956	105
26A	70	5.1	Blr outlet	9.771	5.308	3034	11.77	29.95	1111	106
26B	74	4.6	Mech outlet	.600	.335	201	9.20	45.78	1168	101
28	84	3.9	Blr outlet, 4" O.F. air	20.476	11.929	8026	9.57	37.32	1308	99
29	85	3.8	Blr outlet, 9" O.F. air	15.405	9.027	5839	9.12	35.95	1258	101

Location A



DATA

ISOKINETICS = 111.4.

TEST NUMBER 3

	<u>Vac</u> <u>in. Hg</u>	<u>ft³/min</u>
Before		
After		

DATE 8/4/77

OPERATOR DEC + RAI

FUEL Stinsonbury

SITE A

PROBE LOCATION 4th St

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F						O ₂ , %	Vac.
		Δ P _s	Δ H	Meter Reading	Stack	Probe	Oven	Impingers		Meter		
								In	Out			
1		.17	1.02	523.4	390	350	330		90	120		8
2		.17	1.02		410	340	300		80	120		7
3		.09	0.65		410	340	300		70	120		5
4		.19	1.35		420	330	250		80	125		10
5		.20	1.4		420	340	280		75	130		10
6		.13	0.9		420	360	240		80	120		7
7		.19	1.35	535.78	390	320	230		40	130		9.5
8		.17	1.2		410	320	250		80	140		9
9		.24	1.5		420	330	270		80	130		10
10		.19	1.3	546.15	400	320	270		80	130		7
11		.12	1.1		420	330	290		80	130		8
12		.14	1.0		420	340	200		80	140		9
13		.17	1.2	546.43	410	330	310		80	140		9
14		.17	1.2		420	330	320		80	140		9
15		.22	1.5		420	330	320		80	145		10
16		.16	1.1	552.81	400	320	280		90	150		8
17		.21	1.4		420	330	280		80	140		11
18		.17	1.2		420	330	300		80	140		10
19		.12	.9	557.07	380	350	330		85	150		7.5
20		.19	1.4		400	350	330		85	150		10
21		.22	1.4		410	350	330		85	150		11
				562.00								
Average		.1728	1.19	38.60	410							

METER VOL.	END	567.00
	START	523.40
SAMPLE VOL.		40.69 ft ³ . corr.

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
		23.59

Percent O₂ =

Nomograph Setup

$P_{\text{meter}} = C =$
 $P_{\text{stack}} = T_{\text{stack}} = 400$
 $T_{\text{meter}} = \Delta P =$
 $\Delta H_g = \text{Noz (Ideal)} = 42$
 $\text{H}_2\text{O} = \text{Noz (Actual)} = 327$
 $= .265$

Imp.	Vol. (End)	Vol. (Start)	Δ Vol. (ml)
#1	150	100	50
#2	105	100	5
#3	0	0	0
		Total	55
#4	g(End)	g(Start)	Δ grams
Silica Gel	171.2	159.8	11.4
		Total Vol. H ₂ O	66.4 ml

PARTICULATE

DATA

Leak Check Rate

ISOKINETICS = 99.0%

TEST NUMBER 4

Sampling Time Per Point, Min
2

Vac
in. Hg ft³/min
Before 14.6 0.000
After

DATE 8/17/77
OPERATOR RAP
FUEL Stansbury coal
SITE A
PROBE LOCATION mech out

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F							O ₂ , %	Vac.
		Δ P _s	Δ H	Meter Reading	Stack	Probe	Oven	Impingers		Meter			
								In	Out				
1	12:17	.10	1.32	564.0	425	280	330	S	100	115		11.2	
2		.24	1.35	565.9	425	270	330		95	115		—	
3		.14	.90	—	420	285	325		92	115		7.5	
4	12:27	.16	1.05	569.26	400	295	330		95	118		8.5	
5		.27	1.35	571.19	435	295	325		95	118		11.2	
6		.26	1.35	573.10	430	300	320		95	118		11.0	
7	12:38	.27	1.40	574.98	410	300	315		95	120		11.0	
8		.23	1.40	576.89	418	310	320		92	120		11.0	
9		.21	1.30	578.74	440	305	315		85	120		10.3	
10	12:41	.12	.75	580.24	400	300	300		92	125		6.2	
11		.14	.90	581.73	440	300	300		90	125		7.3	
12		.14	.90	583.32	450	305	300		90	125		7.3	
13	12:58	.29	1.40	585.72	430	300	300		88	125		11.0	
14		.23	1.40	587.13	450	305	300		88	125		10.8	
15		.21	1.30	588.95	450	310	310		80	128		10.0	
16	13:06	.14	.90	590.48	425	310	305		80	129		6.9	
17		.26	1.43	592.41	450	310	305		80	130		10.8	
18		.26	1.42	594.32	450	310	305		78	130		10.8	
19	13:15	.29	1.42	596.24	440	305	305		78	130		10.8	
20		.21	1.30	598.04	450	305	305		78	130		10.0	
21		.11	.70		450	305	305		78	135		5.5	

Nomograph Setup

METER VOL. END 599.592
START 562.112
SAMPLE VOL. 37.271 ft³unc.*

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
1.837		24.03

Percent O₂ =

Corr. Vol. 39.1944 ft³

P_{meter} = C =
P_{stack} = T_{stack} =
T_{meter} = ΔP =
ΔHg = Noz(Ideal) =
% H₂O = Noz(Actual) = 3.77

Imp. Vol. (End) Vol. (Start) ΔVol. (ml)
#1 135 - 100 = 35
#2 115 - 100 = 15
#3 1 - 0 = 1
Total 51
#4 g(End) g(Start) Δgrams
Silica 24.5 - 24.5 = 13.0
Gel
Total Vol. H₂O 64 ml

DATA

Sampling Time Per Point, Min
3

Leak Check Rate

ISOKINETICS =

TEST NUMBER 5
DATE 8/18/77
OPERATOR RAP
FUEL STANBURY
SITE A
PROBE LOCATION Mech. Out

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F						O ₂ , %	Vac.
		Δ P _s	Δ H	Meter Reading	Stack	Probe	Oven	Impingers		Meter		
								In	Out			
1	11:51	.32	1.03	602.18	435	280	310		85	103		9.2
2	*	.24	.78	604.36	470	280	310		75	102		7.0
3		.12	.37	—	465	295	310		72	105		4.0
4	12:04	.17	.53	607.66	450	245	320		75	105		5.5
5		.29	.90	610.05	470	300	320		75	110		8.5
6		.30	.93	612.44	470	310	320		72	110		9.2
7	12:16	.32	.98	614.88	465	305	305		75	112		10.2
8		.25	.78	617.05	470	310	305		75	114		7.6
9		.20	.62	—	470	315	310		75	115		6.5
10	12:27	.13	.41	620.51	470	310	320		78	118		4.8
11		.12	.39	622.05	460	310	315		73	120		4.7
12		.15	.45	623.63	450	310	315		75	120		5.2
13	12:40	.30	.93	626.03	450	300	320		75	125		9.2
14		.26	.80	628.21	455	305	320		72	125		8.2
15		.19	.58	630.00	455	310	320		72	125		6.3
16	12:54	.16	.49	631.69	440	290	310		80	130		5.6
17		.27	.84	633.96	445	295	310		75	130		8.5
18		.27	.84	636.23	480	300	310		72	132		8.8
19	13:06	.28	.87	638.47	435	295	305		75	132		9.0
20		.25	.78	640.58	445	300	310		72	135		8.2
21		.11	.34	642.084	435	300	310		75	135		
Average		.224	.697		452							

METER VOL.	END	642.054
	START	549.541
SAMPLE VOL.		42.54 ft ³ inc.

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
1837		23.99

Percent O_2 = _____

corr. vol. 44. 737 6+

Nomograph Setup

$P_{\text{meter}} = C = 47$
 $P_{\text{stack}} = T_{\text{stack}} = 430$
 $T_{\text{meter}} = \Delta P =$
 $\Delta H_g = 91$ Noz(Ideal) =
 $\% H_2O = 93$ Noz(Actual) = .317

7-58

Imp.	Vol. (End)	Vol. (Start)	ΔVol. (ml)
#1	157	100	57
#2	108	100	8
#3	0	0	0
		Total	65
#4	g(End)	g(Start)	Δgrams
Silica Gel	244.0	233.4	10.6
		Total Vol. H ₂ O	75.6 ml

PARTICULATE

DATA

Leak Check Rate

ISOKINETICS = 108

TEST NUMBER 6
DATE 8/18/77
OPERATOR RALPH GLM
FUEL Stearnsbury
SITE A
PROBE LOCATION mech. out

Sampling Time
Per Point, Min
3

Vac
in. Hg ft³/min
Before 15 0.00
After

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F						O ₂ , %	Vac.
		ΔP _s	ΔH	Meter Reading	Stack	Probe	Oven	Impingers		Meter		
								In	Out			
1	15:36	.35	1.09	644.82	445	320	296		75	112		9.3
2		.27	.85	647.21	445	320	285		65	112		7.2
3		.14	.43	648.84	430	315	280		65	112		4.5
4	15:49	.21	.65	650.90	440	300	275		69	115		6.0
5		.33	1.02	653.46	450	300	280		65	115		8.7
6		.31	.98	655.90	450	300	280		65	115		7.4
7	16:04	.35	1.09	658.60	460	290	290		72	120		9.3
8		.26	.82	660.82	460	285	295		65	120		7.2
9		.26	.82	663.13	460	300	300		65	120		7.2
10	16:15	.15	.46	664.79	460	300	300		70	122		4.5
11		.14	.43	666.46	470	300	300		70	122		4.5
12		.18	.56	668.34	410	300	305		70	125		5.2
13	16:25	.37	1.16	670.90	460	300	310		71	125		10.2
14		.30	.93	673.30	480	305	310		70	128		8.8
15		.28	.87	675.50	430	305	310		70	128		8.2
16	16:38	.18	.56	677.38	470	300	320		75	130		6.2
17		.32	.98	679.72	485	300	315		72	130		10.0
18		.30	.93		470	305	310		72	132		9.4
19	16:52	.37	1.15	682.57	480	295	315		75	133		11.5
20		.29	.90	686.84	480	295	310		75	133		9.8
21		.12	.34	688.325	455	295	310		78	135		4.8
Average												
		.261	.81		457							

Nomograph Setup

METER VOL. END 684.335
START 642.209
SAMPLE VOL. 42.127 ft³ UNC.

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
.83	23.68	23.99

Percent O₂ = 5.8

Corr. Vol. 41.507 ft³

P_{meter} = C
P_{stack} = T_{stack} = 450
T_{meter} = ΔP
ΔH_g = .91 Noz(Ideal) =
% H₂O = 9.4 Noz(Actual) = .817

γ = .60

Imp.	Vol. (End)	Vol. (Start)	ΔVol. (ml)
#1	165	100	65
#2	108	100	8
#3	1	0	1
Total			74
#4	g(End)	g(Start)	Δgrams
Silica Gel	246.3	235	11.3
Total Vol. H ₂ O			85.3 ml

PARTICULATE

DATA

Leak Check Rate

ISOKINETICS = 95

TEST NUMBER 10

Sampling Time
Per Point, Min
3

Vac
in. Hg ft³/min
Before 15" 0.00
After

DATE 8/24/77
OPERATOR RAO
FUEL Stearnsburg Coal
SITE A
PROBE LOCATION 4th St

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F						O ₂ , %	Vac.
		ΔP _s	ΔH	Meter Reading	Stack	Probe	Oven	Impingers		Meter		
								In	Out			
1	10:15	.17	.90	691.18	390	280	320		82	92		2.0
2		.14	.174	693.41	395	280	325		65	95		2.2
3		.07	.37	694.97	395	280	320		65	100		3.6
4	10:30	.09	.48	696.74	390	280	320		65	100		4.5
5		.17	.90	699.22	395	280	310		65	100		7.3
6		.17	.90	701.58	390	290	280		65	102		7.5
7	10:40	.18	.97	704.12	380	280	300		70	102		7.8
8		.15	.80	706.31	400	280	270		68	105		6.5
9		.12	.64	708.49	375	275	305		75	110		5.3
10	10:58	.13	.69	710.57	390	280	310		67	110		5.5
11		.10	.54	712.44	400	290	325		65	100		5.0
12		.12	.64	714.46	360	310	335		70	115		5.4
13		.20	1.08	717.53	390	300	320		70	118		8.3
14		.16	.87	719.78	410	310	335		75	115		7.9
15		.16	.87	722.08	375	320	335		65	115		6.1
16		.08	.49	723.70	380	300	325		72	120		4.1
17		.17	.92	726.05	410	315	320		75	110		7.1
18		.17	.92	728.37	400	320	325		75	120		7.1
19	11:42	.19	1.03	730.73	400	310	315		80	120		8.0
20		.14	.176	732.81	410	315	330		70	120		6.0
21		.08	.43	734.39	400	300	315		75	120		3.9
Average												
		.141	.759		392.1							

Nomograph Setup

METER VOL. END 734.19
START 681.623
SAMPLE VOL. 45.768 ft³ unc.
C_{pitot} Stack Press. Barometric Pressure
83 23.65 23.81
Percent O₂ = 9.9

P_{meter} = C =
P_{stack} = T_{stack} =
T_{meter} = ΔP =
ΔH_g = Noz (Ideal) =
H₂O = Noz (Actual) = 377

Imp. Vol. (End) Vol. (Start) ΔVol. (ml)
#1 136 - 100 = 36
#2 105 - 100 = 5
#3 0 - 0 = 0
Total 41
#4 g (End) g (Start) Δgrams
Silica Gel 222.0 - 209.7 = 12.3
Total Vol. H₂O 57.3 ml

Corr. vol. 47.937 ft³

DATA

ISOKINETICS - 102.

TEST NUMBER 14

DATE 8/26/77

OPERATOR RT + RAP

FUEL STANBURY

SITE A

PROBE LOCATION *Mech. 05*

[illegible]

3

	Vac in. Hg	ft ³ /min
Before	15"	0.00
After		

[illegible]

Nomograph Setup

METER VOL. END 780.762

START 736.808

SAMPLE VOL. 43.454 ft³ unc.

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
.83	23.50	23.77

Percent O_2 = 3.4

corr. vol. 46.222 64³

$P_{meter} = C =$

$P_{meter} = C =$

$P_{stack} = T_{stack}$

$$T_{\text{meter}} = \Delta P$$
$$\Delta H_g = \text{Noz (Ideal)}$$
$$H_2O = \text{Noz (Actual)}$$

7-11

Imp.	Vol.(End)	Vol. (Start)	Δ Vol.(ml)
------	-----------	--------------	-------------------

#1 165 - 100 = 65

第2 110 - 100 - 10

#3 0 - 0 - 0

Total 75

#4	g(End)	g(Start)	Δq_{grams}
----	--------	----------	---------------------------

Silica 158.5 - 150.6 - 8.1

Total Vol. H₂O 83.1 ml

PARTICULATE

DATA

Leak Check Rate

ISOKINETICS = 99.1

TEST NUMBER 15

Vac
in. Hg ft³/min

DATE 8/27/77

OPERATOR RAP

FUEL STANBURY

SITE A

PROBE LOCATION Mech out

Sampling Time Per Point, Min
3

Before

After

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F							O ₂ , %	Vac.
		Δ P _s	Δ H	Meter Reading	Stack	Probe	Oven	Impingers		Meter			
								In	Out				
1	11:27	.30	.82	784.16	440	300	310		86	105		6.7	
2		.27	.75	786.35	440	305	320		68	108		5.7	
3		.13	.35	787.82	390	290	300		90	112		3.4	
4	12:10	.18	.48	—	440	310	330		75	115		4.2	
5		.33	.87	791.87	450	310	310		70	112		6.7	
6		.32	.85	794.20	445	295	310		68	112		6.5	
7	12:27	.34	.91	—	445	305	300		72	118		6.8	
8		.29	.78	798.65	460	305	315		75	118		5.9	
9		.21	.57	800.51	460	320	320		68	120		4.7	
10		.21	.57	802.48	455	300	310		70	122		4.7	
11		.15	.40	803.87	465	310	310		72	123		3.5	
12		.18	.52	805.62	465	305	305		72	125		4.5	
13	12:54	.35	.94	807.99	465	290	310		70	125		7.1	
14		.26	.69	809.97	470	300	300		70	125		5.5	
15		.28	.75	812.10	430	290	300		70	125		5.9	
16	13:08	.17	.46	813.68	470	306	290		70	130		—	
17		.32	.86	815.90	470	300	290		70	130		6.7	
18		.31	.84	818.07	470	300	300		68	132		6.5	
19		.34	.92	820.37	470	300	300		68	135		7.2	
20		.22	.58	822.17	470	290	295		68	135		4.9	
21	12:30	.13	.35	823.564	470	300	290		70	135		3.7	

Nomograph Setup

METER VOL. END 823.564
START 781.750
SAMPLE VOL. 41.814 ft³ Unc.

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
.83	23.54	23.81

Percent O₂ = 45corr. vol. 43.97264³

P_{meter} = C =
P_{stack} = T_{stack} =
T_{meter} = ΔP =
ΔH_g = Noz(Ideal) =
H₂O = Noz(Actual) = .317

T = .69

Imp.	Vol. (End)	Vol. (Start)	ΔVol. (ml)
#1	154	100	54
#2	106	100	6
#3	1	0	1
Total			61
#4	g(End)	g(Start)	Δgrams
Silica Gel	165.9	154.7	11.2
Total Vol. H ₂ O			72.2 ml

PARTICULATE

DATA

Leak Check Rate

ISOKINETICS = 94

TEST NUMBER 16A

Vac
in. Hg ft³/min

DATE 8/30/77

OPERATOR RAP & RT

FUEL STANJUR 4 + kerosene

SITE A

PROBE LOCATION neck out

Sampling Time Per Point, Min
3

Before
After

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F						O ₂ , %	Vac.
		ΔP _s	ΔH	Meter Reading	Stack	Probe	Oven	Impingers		Meter		
1	12:18	.25	.68	827.47	420	290	360		80	150		6.0
2		.23	.64	829.34	430	295	370		80	150		5.8
3		.10	.27	830.51	420	295	370		75	150		3.1
4	12:33	.17	.47	832.11	420	285	350		80	135		4.4
5		.28	.77	834.13	420	295	360		80	125		6.9
6		.27	.74	836.15	400	300	360		75	140		6.8
7	12:48	.28	.77	838.20	410	300	340		75	145		6.9
8		.19	.53	839.85	440	300	350		80	130		5.1
9		.20	.55	841.59	435	300	355		80	140		5.1
10	13:03	.14	.39	843.07	430	300	350		80	140		4.0
11		.20	.55	844.76	440	290	350		80	150		5.1
12		.17	.47	846.39	380	290	310		75	135		4.4
13	13:12	.28	.77	848.42	410	285	340		80	130		6.9
14		.20	.55	850.15	450	290	335		75	125		5.1
15		.24	.66	851.97	400	290	310		70	135		5.9
16	13:30	.16	.44	853.51	400	285	320		80	120		4.3
17		.26	.72	855.49	450	295	315		80	115		6.5
18		.25	.69	857.41	450	295	315		80	130		6.2
19		.27	.74	859.40	430	280	320		80	150		6.7
20		.18	.50	861.01	460	285	320		85	150		4.9
21		.16	.44	862.537	450	290	320		85	130		4.4
Average		.2133	.5876		426							

Nomograph Setup

METER VOL.	END 862.537
	START 825.432
SAMPLE VOL.	37.104 ft ³ UVC.

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
.833	27.46	23.66

Percent O₂ = 6.1corr. Vol. 39.019 ft³

P_{meter} = C =
 P_{stack} = T_{stack} =
 T_{meter} = ΔP =
 ΔH_g = Noz(Ideal) =
 % H₂O = Noz(Actual) =

Imp.	Vol. (End)	Vol. (Start)	ΔVol. (ml)
#1	148	100	48
#2	105	100	5
#3	2	0	2
Total			55

#4	g(End)	g(Start)	Δgrams
Silica	163.8	152.2	11.6
Gel			
Total Vol. H ₂ O			66.6 ml

PARTICULATE

DATA

* Nomograph Change

Nozzle change at point #7
To .248" dia.

Sampling Time Per Point, Min
5

Leak Check Rate

Vac
in. Hg ft³/min
Before 15.0 0.00
After

ISOKINETICS = 102%

TEST NUMBER 16B

DATE 8/30/77

OPERATOR RAP

FUEL Steam + kerosene

SITE A

PROBE LOCATION ESP OUT

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F							O ₂ , %	Vac.
		Δ P _s	Δ H	Meter Reading	Stack	Probe	Oven	Impingers		Meter			
								In	Out				
1	12:00	.42	.155	—	310	340	340		72	75		2.3	
2		.65	.24	623.19	315	350	310		68	78		3.0	
3		.88	.30	625.60	315	300	275		65	80		3.2	
4		.85	.32	628.03	315	360	300		62	82		—	
5		.87	.24	630.17	320	300	300		70	90	*.62	2.8	
6		.62	.17	631.920	315	300	300		65	92		2.3	
				631.980	New Nozzle						*.22		
7		.70	.54	635.11	315	300	280		70	95		4.2	
8	13:00	.94	.82	638.83	315	350	300		70	95		6.0	
9		1.20	1.00	642.95	315	280	300		68	98	*.25	7.5	
10		1.40	1.05	647.13	315	270	300		62	98		7.5	
11		1.30	.97	651.12	315	285	300		62	99		6.9	
12		1.10	.82	654.935	315	285	300		60	100		5.8	
13	13:54	1.3	.97	658.82	315	330	290		65	102		6.7	
14		1.5	1.12	662.06	315	350	300		60	103		7.7	
15		1.70	1.28	667.50	320	320	310		60	102		8.5	
16		1.70	1.28	671.98	320	285	300		60	102		8.5	
17		1.50	1.12	676.20	320	275	300		60	102		7.7	
18		1.20	.90	680.05	315	285	310		62	102		6.2	
19		1.75	1.35	684.89	315	320	280		72	100		9.3	
20		2.10	1.4	—	315	320	295		65	100		9.5	
21		2.50	1.40	694.31	320	230	300		63	100		9.5	
22		1.90	1.40	699.01	315	310	300		62	99		9.5	
23		1.75	1.35	703.69	315	300	300		60	99		9.0	
24		1.35	1.05	705.012	315	290	300		60	100		7.0	
Average		.6937	.2375	1-6	315								
		1.493	1.104	7-24	316								

Nomograph Setup

METER VOL. END 108.012
START 619.072
SAMPLE VOL. ft³

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
1.666	24.06	23.66

Percent O₂ =

P_{meter} = C
P_{stack} = T_{stack}
T_{meter} = ΔP
ΔHg = Noz (Ideal)
H₂O = Noz (Actual) = .187
Y = 5.0

Imp.	Vol. (End)	Vol. (Start)	ΔVol. (ml)
#1	195	100	95
#2	118	100	18
#3	1	0	1
			Total 114
#4	g(End)	g(Start)	Δgrams
Silica Gel	174.8	154.1	20.7
			Total Vol. H ₂ O 174.7 ml

13.986 ft³ Corr. first nozzle
92.768 ft³ " second nozzle

PARTICULATE

DATA

Leak Check Rate

ISO KINETICS = 102%

TEST NUMBER 17A

DATE 8/31/77

OPERATOR JEC

FUEL STAN + Ken coal

SITE A

PROBE LOCATION ESP OUT

Sampling Time Per Point, Min
5

Vac
in. Hg ft³/min
Before 15 0.00
After

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F						O ₂ , %	Vac.
		ΔP _s	ΔH	Meter Reading	Stack	Probe	Oven	Impingers		Meter		
								In	Out			
1	8:28	.60	.16	—	320	350	270		70	73		2.5
2		.54	.14	711.38	315	320	300		65	75		2.2
3		.67	.175	713.08	315	300	320		62	80		2.5
4		.72	.19	714.87	315	285	300		60	82		2.5
5		.62	.165	716.45	315	280	335		58	85		2.3
6		.45	.12	717.81	310	320	320		55	92		2.0
7		.50	.13	719.31	310	350	320		62	98		2.2
8		.65	.17	720.92	310	250	320		62	98		2.3
9	10:27	.85	.22	722.83	310	350	325		62	101		2.8
10		1.0	.26	724.98	310	340	320		62	102		3.3
11		.95	.25	727.12	310	310	330		52	103		3.2
12		.80	.21	729.07	305	305	330		50	108		2.8
13	17:20	1.1	.29	731.24	305	300	300		70	105		5.5
14		1.2	.31	733.65	305	310	320		58	105		3.6
15		1.3	.34	736.15	305	320	320		55	103		3.2
16		1.4	.37	738.64	305	300	300		58	108		4.0
17		1.3	.34	741.07	305	295	340		55	110		2.0
18		1.10	.29	743.30	305	290	325		55	110		3.5
19		1.70	.45	—	305	220	300		65	110		4.5
20	18:10	2.0	.52	744.02	305	350	295		65	110		5.0
21		2.2	.57	752.13	305	200	280		62	110		5.5
22		1.80	.50	755.04	305	290	280		60	110		4.9
23		1.8	.50	757.96	305	290	290		62	110		4.0
24		1.20	.31	760.338	305	285	290		62	110		3.7
Average		1.102	.2908		309							

Nomenclature Setup

METER VOL. END 76.528
START 708.177
SAMPLE VOL. 52.161 ft³ UAC.

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
.666	24.14	23.77

Percent O₂ = 7.3Corr. Vol. = 56.782 ft³

P_{meter} = C =
P_{stack} = T_{stack} =
T_{meter} = ΔP =
ΔHg = Noz(Ideal) =
H₂O = 7.3 Noz(Actual) = 1.88

T = 7.0

Imp. Vol. (End) Vol. (Start) ΔVol. (ml)
#1 160 - 100 = 60
#2 104 - 100 = 4
#3 1 - 0 = 1
Total 65
#4 g(End) g(Start) Agrams
Silica Gel 1726 - 160.9 = 11.7
Total Vol. H₂O 76.7 ml

PARTICULATE

DATA

Leak Check Rate

ISO KINETICS = 104.

TEST NUMBER 170

Vac
in. Hg ft³/min

DATE 8/31/77

OPERATOR GLM

FUEL Stan + Ken coal

SITE A

PROBE LOCATION Stack

* Nomograph change

Sampling Time Per Point, Min
7

Before
After

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F							O ₂ ,%	Vac.
		Δ P _s	Δ H	Meter Reading	Stack	Probe	Oven	Impingers		Meter			
								In	Out				
1	15:41	.22	.29	871.90	160	200	230		54	45		29	
2	15:49	.225	.30	875.32	152	240	260		43	49		3.0	
3	15:57	.28	.37	878.91	168	225	270		35	51		3.4	
4	16:04	.21	.28	882.07	175	275	290		38	52		2.9	
5	16:13	.28	.37	885.73	170	250	300		38	65		3.4	
6	16:25	.275	.50	889.92	150	225	290		48	70	*1.0	—	
7	16:33	.23	.40	894.10	158	210	295		45	65		4.4	
8	16:41	.215	.40	897.702	158	215	315		48	78		3.5	
Avg.		.2419	.3638	897.860	161								
Nozzle change to .316" dia													
1	17:43	.210	.88	903.435	155	220	265		65	75	*.45	7.1	
2	17:52	.220	.90	909.10	157	275	320		68	75		7.3	
3	18:02	.25	.93	914.72	172	250	300		60	65	*.50	7.5	
4		.26	.98	920.440	168	225	300		58	70		7.9	
5	18:18	.31	1.05	926.468	148	240	335		50	80	*.55	8.6	
6		.275	.85	931.766	172	260	290		50	90	*.60	—	
7		.35	1.08	937.628	140	200	300		55	65		8.6	
8	18:45	.25	.7	942.543	172	270	330		58	80	*.66	6.0	
Average													
		.2056	.9213		161								

Nomograph Setup

METER VOL. END 942.543
START 868.56
SAMPLE VOL. ft³

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
.83	27.75	23.75

Percent O₂ = 7.8

P_{meter} = C =
P_{stack} = T_{stack} =
T_{meter} = ΔP =
ΔH_g = Noz(Ideal) =
% H₂O = Noz(Actual) = .2418

P = 1.4

Imp.	Vol. (End)	Vol. (Start)	ΔVol. (ml)
#1	239	100	139
#2	121	100	21
#3	1	0	1
Total			161
#4	g(End)	g(Start)	Δgrams
Silica			
Gel			
Total Vol. H ₂ O			1698 ml

170 Dry gas Vol.
Pt. A 30.644 ft³ (corr. Vol.)
Pt. B 46.989 ft³

PARTICULATE

DATA

Leak Check Rate

ISOKINETICS = 100 %

TEST NUMBER 21

Sampling Time
Per Point, Min
3

Vac
in. Hg ft³/min
Before 15 0.00
After

DATE 9/23/71
OPERATOR JEC
FUEL KEMMERER Cua 1
SITE A
PROBE LOCATION BLR OUT

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F							O ₂ %	Vac.
		Δ P _s	Δ H	Meter Reading	Stack	Probe	Oven	Impingers		Meter			
								In	Out				
1		.03	.23	817.83	680	290	300		90	110		3.0	
2		.22	1.0	820.14	700	350	300		75	110		7.0	
3		.15	.70	822.07	700	450	300		75	110		5.0	
4		.18	.825	824.23	660	400	275		75	110		6.7	
5		.17	.78	825.24	660	530	280		75	115		6.1	
6		.20	.92	825.99	680	330	290		80	115		7.0	
7		.17	.78	826.89	660	330	275		75	115		6.0	
8		.10	.46	827.81	650	340	275		75	120		4.2	
9		.03	.15	828.28	680	330	285		90	120		2.5	
10		.17	.83	829.34	660	300	285		90	120		6.3	
11		.19	.925	830.57	700	340	290		70	120		7.2	
12		.12	.59	831.38	680	360	295		75	120		5.0	
13		.04	.195	831.89	600	350	295		80	120		2.9	
14		.13	.64	832.82	700	350	300		80	120		5.3	
15		.13	.64	833.75	700	370	300		75	120		5.8	
16		.10	.49	834.56	680	370	300		75	120		4.5	
17		.14	.68	835.48	600	350	300		90	120		5.2	
18		.19	.925	836.61	660	350	300		80	120		7.2	
19		.18	.81	837.70	680	375	300		70	120		7.2	
20		.11	.54	838.68	680	385	300		70	120		5.6	
21		.13	.64	839.57	600	360	300		50	125		5.9	
22		.19	.92	840.64	640	370	310		75	125		8.0	
23		.16	.78	841.65	660	380	310		80	125		6.8	
24		.17	.85	842.70	660	385	310		80	130		7.0	
Average		.1425	.6821		661.6								

Nomograph Setup

METER VOL. END 842.70
START 816.68
SAMPLE VOL. 26.02 ft³ unc.

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
.837	23.69	23.74

Percent O₂ =

P_{meter} = C =
P_{stack} = T_{stack} =
T_{meter} = ΔP =
ΔH_g = Noz(Ideal) =
% H₂O = Noz(Actual) = 37C

Imp. Vol. (End) Vol. (Start) ΔVol. (ml)
#1 137 - 100 = 37
#2 105 - 100 = 5
#3 0 - 0 = 0
Total 42
#4 g(End) g(Start) Δgrams
Silica Gel 246.3 - 232.3 = 8.0
Total Vol. H₂O 50.0 ml

Corr. Vol = 29.38

PARTICULATE

DATA

Leak Check Rate

ISOKINETICS = 102.TEST NUMBER 22

Sampling Time Per Point, Min
<u>2</u>

	Vac in. Hg	ft ³ /min
Before	<u>15.0"</u>	<u>0.00</u>
After		

DATE 9/23/77
 OPERATOR RAP
 FUEL Kimmerer
 SITE A
 PROBE LOCATION _____

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F						O ₂ , %	Vac.
		Δ P _s	Δ H	Meter Reading	Stack	Probe	Oven	Impingers		Meter		
								In	Out			
1		.15	.73	844.13	640	300	260	5	90	110		5.0
2		.21	1.0	845.31	660	340	260		60	110		5.3
3		.17	.84	846.40	670	375	290		65	110		5.1
4		.12	.58	847.34	675	390	260		70	110		4.1
5		.19	.93	848.66	630	380	330		75	110		5.9
6		.20	.98	849.84	680	390	340		80	110		6.0
7		.18	.88	850.95	700	400	350		80	110		6.0
8		.12	.59	851.89	680	400	360		80	115		4.7
9		.05	.22	852.47	600	385	360		80	115		2.4
10		.19	.93	853.59	690	390	360		80	120		6.0
11		.18	.88	854.69	720	400	370		85	120		6.0
12		.14	.69	855.68	710	395	375		80	120		5.3
13		.03	.15	856.13	600	360	360		80	120		2.6
14		.23	1.10	857.32	680	335	360		80	120		7.0
15		.20	.98	858.47	700	350	360		80	120		7.0
16		.14	.69	859.41	700	350	360		80	120		5.4
17		.20	.98	860.77	620	330	360		80	120		7.1
18		.21	1.05	861.89	650	330	360		80	120		7.6
19		.20	.98	862.95	670	330	360		80	125		7.0
20		.13	.64	863.80	628	325	360		80	125		5.1
21		.14	.69	865.72	640	310	360		85	125		6.0
22		.23	1.16	868.08	660	330	360		80	130		8.0
23		.17	.83	870.19	680	320	360		80	130		7.0
24		.20	.98	872.41	640	370	360		90	130		7.9
Average												
		.165	.811		663							

Nomograph Setup

METER VOL. END 872.41
START 843.07
 SAMPLE VOL. 29.34 ft³

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
<u>877</u>	<u>23.69</u>	<u>29.74</u>

Percent O₂ = _____

31.9408 corr. Vol

P_{meter} = C =
 P_{stack} = T_{stack} =
 T_{meter} = ΔP =
 ΔH_g = Noz(Ideal) =
 % H₂O = Noz(Actual) = .376

Imp.	Vol. (End)	Vol. (Start)	ΔVol. (ml)
#1	<u>143</u>	<u>100</u>	= <u>43</u>
#2	<u>110</u>	<u>100</u>	= <u>10</u>
#3	<u>0</u>	<u>0</u>	= <u>0</u>
Total			<u>53</u>
#4	<u>g(End)</u>	<u>g(Start)</u>	<u>Δgrams</u>
Silica	<u>213.2</u>	<u>205.6</u>	= <u>7.6</u>
Gel			
Total Vol. H ₂ O			<u>60.6</u> ml

PARTICULATE

DATA

Leak Check Rate

ISOKINETICS = 101%

TEST NUMBER 23

Vac
in. Hg ft³/min

DATE 9/24/77

Sampling Time
Per Point, Min
1.5

Before

After

OPERATOR RAP

FUEL KEMMERER COAL

SITE A

PROBE LOCATION BLR OUT

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F							O ₂ , %	Vac.
		Δ P _s	Δ H	Meter Reading	Stack	Probe	Oven	Impingers		Meter			
								In	Out				
1		.05	.26	873.52	580	320	350		110	120		2.4	
2		.10	.54	874.36	590	350	350		100	125		3.5	
3		.07	.38	875.10	600	380	350		90	125		3.0	
4		.10	.54	875.96	580	400	350		95	125		3.5	
5		.08	.43	876.74	500	390	350		95	125		3.2	
6		.10	.54	877.62	570	370	350		90	125		3.7	
7		.09	.48	878.40	590	365	350		90	130		3.3	
8		.05	.26	879.06	570	350	350		90	130		2.5	
9		.01	.05	879.27	520	335	350		110	130		1.0	
10		.09	.48	880.10	570	330	348		100	130		3.5	
11		.09	.48	880.90	600	350	350		90	130		3.5	
12		.05	.26	881.50	600	360	350		90	130		2.5	
13		.00											
14		.06	.32	882.16	550	360	330		100	130		3.0	
15		.06	.32	882.85	600	360	350		95	130		3.0	
16		.05	.26	883.45	600	370	350		95	130		2.5	
17		.09	.48	884.20	500	370	350		100	135		3.3	
18		.09	.48	884.98	560	370	350		90	135		4.1	
19		.07	.27	885.56	590	380	360		90	135		2.4	
20		.06	.32	886.21	600	370	300		95	140		2.4	
21		.07	.37	886.90	520	370	360		100	140		3.0	
22		.08	.42	887.56	560	370	360		95	140		3.0	
23		.16	.53	888.40	600	370	360		90	140		3.5	
24		.09	.48	889.13	600	380	360		90	140		3.0	
Average		.07	.3891		572.7								

Nomograph Setup

METER VOL. END 189.5
START 72.9
SAMPLE VOL. 116.6 ft³ U.C.

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
877	23.58	23.62

Percent O₂ =

P_{meter} = C =
P_{stack} = T_{stack} =
T_{meter} = ΔP =
ΔH_g = Nox(Ideal) =
% H₂O = Nox(Actual) = 376

Imp.	Vol. (End)	Vol. (Start)	ΔVol. (ml)
#1	111	100	11
#2	114	100	14
#3	0	0	0
			Total 25
#4	g(End)	g(Start)	Δgrams
Silica Gel	156.5	151.8	4.7
			Total Vol. H ₂ O 29.7 ml

Corr. vol. = 17.646 ft³

PARTICULATE

DATA

Leak Check Rate

ISOKINETICS = 105%

TEST NUMBER 24

Vac
in. Hg ft³/min

DATE 9/24/77

Sampling Time
Per Point, Min
1.5

Before
After

OPERATOR R4P

FUEL Kemmerer

SITE A

PROBE LOCATION BLR04

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F						O ₂ %	Vac.
		ΔP _s	ΔH	Meter Reading	Stack	Probe	Oven	Impingers		Meter		
								In	Out			
1	15:29	.08	.43	—	560	340	290	S	75	115		4.0
2		.10	.54	891.01	570	345	300		75	115		4.5
3		.07	.38	891.77	570	300	310		80	116		3.8
4		.09	.48	892.60	580	350	310		73	118		4.1
5	15:45	.09	.48	893.43	570	310	320		80	120		4.3
6		.10	.54	894.32	580	310	320		78	120		4.8
7		.09	.48	895.14	590	315	330		75	121		4.5
8		.06	.33	895.87	580	310	320		75	121		3.7
9		—	—	negative								
10		.08	.43	896.67	570	275	320		85	122		4.2
11		.08	.43	897.46	590	280	320		78	122		4.2
12		.06	.33	898.14	580	285	320		78	122		3.7
13		.02	.011	—	550	270	310		88	123		2.3
14	16:38	.10	.54	899.45	565	270	310		80	125		5.0
15		.10	.54	900.33	590	290	310		79	125		5.0
16		.06	.33	901.04	595	310	310		79	125		3.8
17		.09	.48	—	560	280	310		89	125		4.7
18		.10	.54	902.57	570	295	310		80	125		5.0
19		.09	.48	903.58	580	300	305		80	125		4.8
20		.04	.22	904.13	590	300	300		80	125		3.0
21	16:42	.06	.33	—	560	290	310		90	129		3.3
22		.12	.65	905.80	580	310	310		82	129		5.7
23		.09	.48	906.62	595	320	310		82	129		4.7
24		.10	.54	907.508	580	330	310		85	129		5.1
Average		.0813	.4344		576.7							

Nomograph Setup

METER VOL. END 907.508
START 889.314
SAMPLE VOL. 18.194 ft³UCL

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
837	23.59	23.62

Percent O₂ =

P_{meter} = C =
P_{stack} = T_{stack} =
T_{meter} = ΔP =
ΔH_g = Noz(Ideal) =
% H₂O = Noz(Actual) = .381

Imp. Vol. (End) Vol. (Start) ΔVol. (ml)
#1 130 100 = 30
#2 102 100 = 2
#3 0 0 = 0
Total 32

#4 g(End) g(Start) Δgrams
Silica Gel 158.7 156.5 = 2.2
Total Vol. H₂O 34.2 ml

Corr. Vol. = 19.806 ft³

PARTICULATE

DATA

Leak Check Rate

ISOKINETICS = 106%

TEST NUMBER 26A

* nomograph change

Sampling Time Per Point, Min
1.5

Vac
in. Hg ft³/min

Before
After

DATE 10/6/77

OPERATOR RAP

FUEL Kemmerer Coal

SITE A

PROBE LOCATION BLR OUT

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F							O ₂ , %	Vac.
		Δ P _s	Δ H	Meter Reading	Stack	Probe	Oven	Impingers		Meter			
								In	Out				
1	10:27	.07	.38	908.45	620	270	330	}	100	120		3.5	
2		.18	.97	909.62	620	285	325		90	119		6.0	
3		.15	.80	910.70	625	320	320		70	119		5.2	
4		.15	.80	—	625	325	325		78	119		5.2	
5	10:41	.14	.75	912.83	610	320	320		82	120		5.0	
6		.16	.86	913.92	620	320	320		80	121		5.8	
7		.15	.80	914.99	620	325	320		75	121		5.2	
8		.09	.48	915.83	615	330	330		75	122		3.2	
9		.02	.108	916.24	600	285	320		90	125		2.0	
10		.12	.64	917.20	620	290	320		85	125		4.8	
11		.13	.70	918.15	640	320	325		75	128		5.0	
12		.09	.48	918.96	650	320	320		75	128		4.0	
13	11:22	.01	.05	919.30	600	300	315		100	132	*	6.2	
14		.11	.57	920.10	620	315	315		90	130		4.5	
15		.12	.62	921.03	650	330	320		80	130		4.8	
16		.10	.51	921.870	650	330	320		72	130		4.3	
				922.005	Leak	Check	OK						
17	11:42	.13	.67	923.000	610	270	310	85	130		5.0		
18		.13	.67	923.95	630	270	310	78	131		4.9		
19		.12	.62	924.90	635	275	310	72	130		4.7		
20		.08	.41	925.64	610	270	300	78	132		3.2		
21		.11	.57	926.52	600	275	300	83	132		4.3		
22		.11	.57	927.40	610	275	300	83	132		4.3		
23		.09	.41	928.14	640	290	300	75	132		3.6		
24		.14	.72	929.142	520	310	300	78	133		5.0		
Average		.12	.59		618.7								

Nomograph Setup

METER VOL. END 929.142
START 907.625
SAMPLE VOL. 21.457 ft³ inc.

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
.837	23.73	23.77

Percent O₂ =

P_{meter} = C =

P_{stack} = T_{stack} =

T_{meter} = ΔP =

ΔH_g = Noz(Ideal) =

% H₂O = 9.5 Noz(Actual) = 381

Y = .35

corr. vol. = 23.358 ft³

Imp.	Vol. (End)	Vol. (Start)	ΔVol. (ml)
#1	140	100	40
#2	107	100	7
#3	0	0	0
Total			47
#4	g(End)	g(Start)	Δgrams
Silica Gel	160.6	153.3	5.3
Total Vol. H ₂ O			52.3 ml

PARTICULATE

DATA

Leak Check Rate

ISOKINETICS = 101

TEST NUMBER 26B

Vac
in. Hg ft³/min

DATE 10/6/77

Sampling Time
Per Point, Min

Before

OPERATOR RAP

3

After

FUEL Kemmerer Coal

SITE A

PROBE LOCATION Mech. Out

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F							O ₂ , %	Vac.
		Δ P _s	Δ H	Meter Reading	Stack	Probe	Oven	Impingers		Meter			
								In	Out				
1		.39	1.05	962.740	480	340	310		90	125			
2		.32	.87		480	340	310		75	125			
3		.13	.35		460	340	310		80	130			
4		.18	.50		440	340	300		80	130			
5		.35	.95	979.45	480	330	280		75	130			
6		.33	.90		480	325	290		85	135			
7		.42	1.15	984.83	450	340	300		80	135			
8		.38	1.05		470								
9		.35	.94		480	325	315		83	140			
10		.17	.45	989.73	480	270	300		95	140			
11		.20	.53		480	290	300		85	140			
12		.25	.69		460	310	310		85	145			
13		.40	1.05	995.405	460	300	310		85	145			
14		.38	1.0		480	310	320		85	150			
15		.31	.85		480	315	320		85	150			
16		.15	.399	1002.015	460	315	320		87	150			
17		.39	1.01		475	310	325		85	150			
18		.35	.90		460	315	330		85	150			
19		.38	1.0	1008.420	460	310	330		90	155			
20		.40	1.05		460	310	330		85	155			
21		.18	.45	1014.915	460								

Nomograph Setup

METER VOL. END 1014.915
START 962.740
SAMPLE VOL 46.175 ft³ UHC.

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
.837	23.45	23.77

Percent O₂ =

P_{meter} = C =
P_{stack} = T_{stack} =
T_{meter} = ΔP =
ΔH_g = Noz(Ideal) =
H₂O = Noz(Actual) =

▼ -.68

Imp. Vol. (End) Vol. (Start) ΔVol. (ml.)
#1 165 - 100 = 65
#2 107 - 100 = 7
#3 1 - 0 = 1
Total 73

#4 g(End) g(Start) Δgrams
Silica 170.3 - 160.6 = 9.7
Gel
Total Vol. H₂O 82.7 ml

Corr. Vol. = 42.558 ft³

PARTICULATE

DATA

Leak Check Rate

ISOKINETICS = 99

TEST NUMBER 28

Vac
in. Hg ft³/min

DATE 10/10/77

OPERATOR RAO

FUEL Kemmerer Coal

SITE A

PROBE LOCATION BLR OUT

* nomograph change

Sampling Time
Per Point, Min
1.5

Before
After

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F							O ₂ , %	Vac.
		Δ P _s	Δ H	Meter Reading	Stack	Probe	Oven	Impingers		Meter			
								In	Out				
1	11:43	.17	.78	930.70	650	280	310	7	90	115		7.2	
2		.22	1.13	931.95	665	310	310		75	115		8.2	
3		.18	.93	933.09	685	320	310		70	118		7.0	
4		.19	1.0	934.26	690	330	320		72	118		7.3	
5	11:52	.23	1.20	935.55	670	320	320		73	120		8.5	
6		.22	1.13	936.79	700	330	320		70	120		8.0	
7		.20	.93	—	700	330	325		72	121	*	7.0	
8		.11	.52	938.10	680	320	320		70	122		4.5	
9		.01	1.03	939.07	670	290	320		85	125		5.20	
10		.16	.74	940.10	680	280	320		85	125		5.8	
11		.17	.78	941.12	720	290	320		72	126		6.2	
12		.15	.69	942.10	710	305	305		70	127		5.5	
13		.02	.08	942.43	650	270	310		82	130		2.0	
14	12:21	.22	1.02	943.60	680	270	310		80	130		8.0	
15		.23	1.05	944.78	700	290	310		68	130		8.2	
16		.12	.56	945.64	700	310	310		60	130		5.2	
17		.07	.32	946.32	670	270	300		80	135		3.8	
18		.22	1.02	947.48	695	280	310		70	135		8.0	
19		.21	.98	948.62	690	310	310		62	135		7.6	
20		.11	.52	949.45	690	305	300		63	135		4.8	
21	12:44	.14	.64	950.40	660	280	300		78	140		5.5	
22		.25	1.15	951.61	665	280	300		72	138		8.1	
23		.19	.88	952.70	680	290	300		73	140		7.2	
24		.20	.92	953.78	680	300	300		73	139		7.3	
Average		.1663	.7958		683								

Nomograph Setup

METER VOL. END 953.78
START 929.53
SAMPLE VOL. 24.26 ft³ U.C.

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
.837	23.73	23.78

Percent O₂ =

P_{meter} = C =
P_{stack} = T_{stack} =
T_{meter} = ΔP =
ΔH_g = Noz (Ideal) =
% H₂O = Noz (Actual) = .382
T = .36

Imp. Vol. (End) Vol. (Start) ΔVol. (ml)
#1 136 - 100 = 36
#2 105 - 100 = 5
#3 0 - 0 = 0
Total 41
#4 g (End) g (Start) Δgrams
Silica Gel 62.4 - 157.4 = 6
Total Vol. H₂O 47 ml

Corr. Vol. = 26.4134 ft³

PARTICULATE

DATA

Leak Check Rate

ISO KINETICS = 101%

TEST NUMBER 251

Vac
in. Hg ft³/min

DATE 10/10/77

Sampling Time
Per Point, Min
1.5

Before

OPERATOR RAP

After

FUEL Kammeter Coal

SITE A

PROBE LOCATION BLR OUT

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F						O ₂ , %	Vac.
		Δ P _s	Δ H	Meter Reading	Stack	Probe	Oven	Impingers		Meter		
								In	Out			
1		.09	.45	954.77	660	285	310	5	90	130		4.0
2	14:35	.24	1.20	956.02	665	300	310		88	128		7.8
3		.19	.95	957.17	680	330	310		80	130		6.3
4		.21	1.05	958.37	670	330	320		78	130		7.0
5		.08	.40	959.12	670	285	320		88	130		3.7
6		.24	1.20	960.39	680	275	320		80	130		7.1
7	14:50	.22	1.10	961.61	680	295	310		75	130		7.2
8		.12	.60	962.51	665	300	315		75	132		4.5
9		.03	.15	963.00	660	260	305		90	132		2.5
10	15:02	.18	.90	964.10	680	270	305		85	133		6.2
11		.21	1.05	965.29	700	305	305		72	133		7.0
12		.13	.65	966.23	685	325	305		70	133		4.8
13	15:13	.03	.15	966.74	680	270	315		80	136		2.5
14		.18	.90	967.88	710	300	290		76	135		6.8
15		.16	.80	968.89	730	330	300		70	138		5.3
16		.14	.70	969.89	710	340	300		68	135		5.0
17		.08	.40	970.64	680	315	300		78	140		3.7
18		.22	1.10	971.84	690	310	300		75	140		7.2
19		.19	.95	972.96	710	295	310		72	140		6.2
20		.12	.60	973.87	690	340	305		70	140		4.5
21	15:40	.07	.35	974.56	670	315	300		80	142		3.5
22		.22	1.10	975.73	680	315	300		75	142		7.2
23		.16	.80	976.76	700	315	300		70	142		5.8
24		.21	1.05	977.885	700	340	300		70	142		7.0
Average		1.550	.7750		685							

Nomograph Setup

METER VOL. END 977.885

START 953.950

SAMPLE VOL. 23.435 ft³/min

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
.837	23.74	23.80

Percent O₂ =

P_{meter} = C =
 P_{stack} = T_{stack} =
 T_{meter} = ΔP =
 ΔH_g = Noz(Ideal) =
 % H₂O = Noz(Actual) = .362

= .37

Imp. Vol. (End) Vol. (Start) ΔVol. (ml)
 #1 135 - 100 = 35
 #2 102 - 100 = 2
 #3 0 - 0 = 0
 Total 37

#4 g(End) g(Start) Δgrams
 Silica Gel 170.4 - 163.4 = 7.0
 Total Vol. H₂O 44 ml

Corr. Vol. = 26.0556

72

DATA

Load dropped
from 95-760g after
9 points. Sampling continued
for ash sample only.

Sampling Time Per Point, Min	3.5
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Leak Check Rate

Vac
in. Hg ft³/min

Before

After

ISOKINETICS =

TEST NUMBER 33
DATE 10/16/77
OPERATOR PLL + RAP
FUEL Kommerov
SITE A
PROBE LOCATION BLR 05

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F						O ₂ , %	Vac.
		Δ P _s	Δ H	Meter Reading	Stack	Probe	Oven	Impingers		Meter		
								In	Out			
1	11:13	.09	.47	979	660	265	320		82	118		3.8
2		.24	1.25	993.00	670	335	320		62	118		7.4
3		.17	.88	985.70	670	285	365		62	119		6.8
4	11:30	.21	1.10	988.60	670	355	320		64	120		7.0
5	11:33	.03	.157	989.7	640	325	302		73	123		2.5
6		.22	1.15	992.6	670	333	310		70	125		7.0
7		.22	1.15	995.5	685	365	311		67	122		7.0
8		.13	.675	997.7	665	365	322		70	130		4.8
Port 4	4											
	15 min.	.21	1.10	1009.6	670	303	335		88	131		7.0
Port 3	3											
	20 min.	.21	1.10	1025.5	670	330	320		80	143		7.0
Port 2												
	14:43	.13	.18	1034.6								
Port 2		.11	1.6	1067.80	615	310	330		72	155		10.0
1/2 inch nozzle max 50 H ₂ O												
Average												

METER VOL.	END	067.96
	START	978.000
SAMPLE VOL.		

C_{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
427		

Percent O_2 =

Nomograph Setup

P_{meter}	=	C	=
P_{stack}	=	T_{stack}	=
T_{meter}	=	ΔP	=
ΔH_g	=	$Noz(Ideal)$	=
% H_2O	=	$Noz(Actual)$	=

Imp.	Vol. (End)	Vol. (Start)	ΔVol. (ml)
#1	_____	- _____	= _____
#2	_____	- _____	= _____
#3	_____	- _____	= _____
		Total	_____
#4	<u>g(End)</u>	<u>g(Start)</u>	<u>Δgrams</u>
Silica	_____	_____	_____
Gel	_____	- _____	= _____
		Total Vol. H ₂ O	_____ ml

PARTICULATE

DATA

Leak Check Rate

ISOKINETICS = 96

TEST NUMBER 34A

Sampling Time Per Point, Min
3.0

	Vac in. Hg	ft ³ /min
Before	15"	0.00
After	15"	0.00

DATE 10/29/77
 OPERATOR JEC
 FUEL Consolidation Coal
 SITE A
 PROBE LOCATION BLDOJ

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F							O ₂ , %	Vac.
		Δ P _s	Δ H	Meter Reading	Stack	Probe	Oven	Impingers		Meter			
								In	Out				
1		.06	.31	1087.25	600	280	350		100	125		2	
2		.15	.75	1088.74	600	320	350		90	125		4	
3		.14	.70	1090.71	640	350	345		80	125		5	
4		.07	.35	1092.65	620	350	345		90	130		2	
5	12:08	.04	.20	1093.99	600	300	340		100	130		1.5	
6		.16	.80	1095.11	620	330	340		90	130		5	
7		.15	.75	1097.12	610	350	345		90	133		5	
8		.10	.57	1099.08	600	350	340		85	135		4.3	
9		.10	.57	1100.71	620	360	230		100	135		4.5	
10		.17	.85	1102.30	640	320	300		95	140		6.5	
11		.14	.70	1104.10	640	350	300		90	140		6	
12		.15	.75	1106.17	620	350	200		95	140		6	
13		.08	.40	1108.10	600	280	330		100	130		4.5	
14		.16	.80	1109.57	620	300	330		100	130			
15		.13	.66	1111.68	630	350	330		85	130		6.5	
16		.14	.70	1113.52	600	350	330		85	130		7.0	
17		.14	.70	1115.45	620	300	330		90	125		7.0	
18		.17	.80	1117.35	600	330	320		80	120		7.5	
19		.15	.75	1119.74	610	320	220		80	120		7.0	
20		.19	.90	1121.85	600	330	320		70	120		9.0	
21		.05	.25	1124.05	600	300	330		85	125		3	
22		.20	1.10	1125.23	620	330	320		80	125		9	
23		.14	.95	1127.25	640	360	330		80	125		9	
24		.15	.75	1130.15	620	380	350		80	125		7.5	
			Final	1132.17									
Average		.132	.664		615								

Nomograph Setup

METER VOL. END 1132.17
 START 1087.25
 SAMPLE VOL. 44.92 ft³ UMC

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
.837	23.64	23.69

Percent O₂ =

P_{meter} = C =
 P_{stack} = T_{stack} =
 T_{meter} = ΔP =
 ΔH_g = Noz(Ideal) =
 % H₂O = 15 Noz(Actual) = 3.87

T = 370

Imp.	Vol. (End)	Vol. (Start)	ΔVol. (ml)
#1	170	100	70
#2	50	100	-50
#3	10	0	10
Total			30
#4	g(End)	g(Start)	Δgrams
Silica	166	150	16
Gel			
Total Vol. H ₂ O			46 ml

Corr. Vol. = 48.90 ft³

PARTICULATE

DATA

Leak Check Rate

ISOKINETICS = 106

TEST NUMBER 348

Vac
in. Hg ft³/min

DATE 10/29/77

Sampling Time
Per Point, MinBefore 15.0 002
After

OPERATOR RAP

FUEL Consolidation

SITE A

PROBE LOCATION ESP OUT

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F							O ₂ , %	Vac.
		Δ P _s	Δ H	Meter Reading	Stack	Probe	Oven	Impingers		Meter			
								In	Out				
1	11:27	.52	.135	1801.52	345	340	310		68	Temp		<2.0	
2		.68	.18	1803.31	350	320	310		62	Comp.		<2.0	
3		.94	.245	1805.39	350	300	310		60	530°R		<2.0	
4		1.20	.31	1807.77	350	290	310		60			2.2	
5		1.10	.29	1809.90	350	305	305		59			2.0	
6		.91	.24	1811.91	350	310	305		60			<2.0	
TEMPORARY SHUTDOWN TO Allow SASS start up													
7	13:14	1.05	.28	1814.20	350	320	290		60			2.2	
8		1.28	.34	1816.77	355	320	290		58			2.5	
9		1.55	.41	1819.54	350	290	290		57			2.8	
10		1.95	.52	1822.69	355	290	295		53			3.2	
11		1.75	.46	1825.57	355	290	290		48			3.0	
12		1.40	.37	1828.16	355	275	290		45			2.7	
13	14:31	1.55	.41	1831.08	350	320	320		50			2.8	
14		1.75	.46	1834.06	350	315	315		48			3.0	
15		2.05	.54	1837.31	350	290	315		48			3.5	
16		2.25	.62	1840.71	350	300	315		48			3.8	
17		1.80	.47	1843.62	355	300	320		48			3.0	
18		1.75	.46	1846.49	355	300	320		45			2.8	
19		2.25	.62	1848.81	360	300	310		58			3.8	
20		2.80	.74	1853.52	360	320	320		52			4.2	
21		3.0	.80	1857.39	360	310	320		50			4.5	
22		2.7	.72	1861.08	365	290	290		50			4.0	
23		2.1	.56	1864.31	370	240	310		53			3.5	
24	15:50	1.85	.49	1867.260	365	245	300		53			3.2	
Average		1.674	.444		354								

Nomograph Setup

METER VOL. END 1867.260

START 1794.745

SAMPLE VOL. 67.465 ft³ u.c.

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
.666	24.07	23.69

Percent O₂ =

P_{meter} = C =
P_{stack} = T_{stack} =
T_{meter} = ΔP =
ΔH_g = Noz(Ideal) =
% H₂O = Noz(Actual) = .189

T = 7.0

Imp. Vol. (End) Vol. (Start) ΔVol. (ml)
#1 175 - 100 = 75
#2 110 - 100 = 10
#3 0 - 0 = 0
Total 85

#4 g(End) g(Start) Δgrams
Silica Gel 162.0 - 150.0 = 12
Total Vol. H₂O 97 ml

Corr. Vol = 70.562 ft³

PARTICULATE

DATA

Leak Check Rate

ISOKINETICS = 100

TEST NUMBER 35A

DATE 10/30/77

OPERATOR SEC

FUEL Consolidation Coal

SITE A

PROBE LOCATION BLR05

Sampling Time
Per Point, Min

Vac
in. Hg ft³/min
Before 16 0.00
After 16 0.00

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F							O ₂ , %	Vac.
		Δ P _s	Δ H	Meter Reading	Stack	Probe	Oven	Impingers		Meter			
								In	Out				
1		.02	.10	1132.91	620	270	350			85	100		1
2		.21	1.1	1132.80	650	320	350			75	105		6
3		.19	.95	1136.21	610	360	350			70	105		6
4		.13	.65	1138.67	650	380	350			70	110		4.5
5		.03	.15	1140.57	620	710	340			80	110		1
6		.22	1.1	1141.59	640	300	330			75	110		7
7		.20	1.0	1144.05	660	350	330			70	110		6
8		.16	.80	1146.45	640	340	330			70	110		—
9		.08	.40	1148.54	640	280	330			75	115		2.5
10		.21	1.1	1150.2	650	290	330			70	115		6.5
11		.17	.85	1152.42	650	330	330			70	115		5
12		.18	.90	1154.60	610	330	330			75	115		6
13		.14	.71	1156.81	620	280	300			70	110		5
14		.20	1.0	1158.97	640	300	330			65	110		6.2
15		.17	.85	1161.5	650	340	330			60	110		17.5
16		.19	.95	1163.52	630	220	330			70	115		—
				1165.832		Leak Check - OK							
17		.12	.65	1167.19	650	260	310			90	110		—
18		.17	.96	1169.18	660	300	320			80	110		6.0
19		.16	.80	1171.33	660	330	330			75	115		5.0
20		.10	.51	1173.47	610	240	330			80	115		3.0
21		.03	.16	1175.20	620	260	330			90	115		1.0
22		.15	.26	1176.12	660	330	340			70	120		5
23		.18	.90	1178.41	660	340	340			70	120		—
24		.14	.70	1180.64	660	340	340			70	120		5
Average		.148	.748	1182.600	643								

Nomograph Setup

METER VOL. END 1192.60
START 1132.91
SAMPLE VOL. 49.69 ft³ UNC

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
.837	23.57	23.62

Percent O₂ =

P_{meter} - C =

P_{stack} = T_{stack} =

T_{meter} = ΔP =

ΔH_g = Noz (Ideal) =

% H₂O = Noz (Actual) = .381

Y = .37

Corr. Vol. = 52.66 ft³

Imp. Vol. (End) Vol. (Start) ΔVol. (ml)

#1 120 - 100 = 20

#2 125 - 100 = 25

#3 22 - 0 = 22

Total 67

#4 g(End) g(Start) Δgrams

Silica Gel 1515 - 150.7 = 1.5

Total Vol. H₂O 68.5 ml

PARTICULATE

DATA

Leak Check Rate

ISOKINETICS - 105'

TEST NUMBER 35B

Vac
in. Hg ft³/min

DATE 10/30/77

Sampling Time
Per Point, Min

Before

OPERATOR RAP

5

After

FUEL Consolidation

SITE 4

PROBE LOCATION 61P OUT

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F							O ₂ %	Vac.
		Δ P _s	Δ H	Meter Reading	Stack	Probe	Oven	Impingers		Meter			
								In	Out				
1	13:01	.28	.20	1869.66	360	310	310		45	TEMP		2.0	
2		1.20	.31	1872.17	365	300	290		45	COMP		2.2	
3		1.65	.42	1875.06	365	310	290		42	530°R		2.1	
4		1.80	.46	1870.06	365	290	300		42			2.1	
5		1.70	.43	1880.91	370	290	310		42			2.7	
6		1.05	.27	1883.16	365	290	320		42			2.2	
7	13:51	1.25	.32	1885.66	365	305	310		52			2.3	
8		1.80	.46	1888.57	365	320	290		50			2.7	
9		2.30	.58	1891.52	370	320	300		48			3.1	
10		2.65	.67	1895.30	370	300	300		45			3.7	
11		2.40	.62	1898.59	365	285	310		45			3.4	
12		1.65	.42	1901.33	365	295	310		43			2.1	
13	14:08	1.65	.42	1904.12	370	285	320		48			2.7	
14		1.85	.47	1907.00	365	320	300		47			2.9	
15		2.30	.59	1910.25	370	320	320		45			3.3	
16		2.70	.69	1913.71	370	310	320		45			3.7	
17		1.95	.50	1916.68	370	300	320		43			2.9	
18		1.70	.43	1919.46	370	290	315		45			2.1	
19		2.30	.59	1922.58	370	310	285		48			3.2	
20		2.6	.66	1926.50	370	310	285		48			3.8	
21		3.20	.82	1930.09	370	270	290		37			4.3	
22		3.70	.95	1934.33	370	300	300		42			5.0	
23		3.55	.90	1938.46	370	310	310		42			4.8	
24		3.0	.76	1942.262	370	310	310		42			4.2	
Average		2.11	.539		367.7								

Nomograph Setup

METER VOL. END 1944.92

START 1862.72

SAMPLE VOL. 74.65 ft³ UMC.

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
.666	24.11	23.63

Percent O₂ =

P_{meter} = C
 P_{stack} = T_{stack}
 T_{meter} = ΔP
 ΔH_g = Noz(Ideal)=
 % H₂O = Noz(Actual)=.198

T = 7.2

Corr. Vol = 78.115 ft³ dry

Imp.	Vol. (End)	Vol. (Start)	ΔVol. (ml)
#1	180	100	80
#2	112	100	12
#3	.5	0	.5
			Total 92.5
#4	g(End)	g(Start)	Δgrams
Silica Gel	164	150	14
			Total Vol. H ₂ O 1065 ml

PARTICULATE

DATA

Leak Check Rate

ISO KINETICS = 103

TEST NUMBER 26

Vac
in. Hg ft³/min

DATE 11/1/77

OPERATOR RAP

FUEL Consolidation Coal

SITE A

PROBE LOCATION BLR OUT

Sampling Time
Per Point, Min
1.5

Before 15.0 0.00
After

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F						O ₂ %	Vac.
		Δ P _s	Δ H	Meter Reading	Stack	Probe	Oven	Impingers		Meter		
								In	Out			
1	10:18	.12	.59	1184.70	620	280	300	7	82	110		4.6
2		.15	.74	1185.75	620	290	300		82	110		5.1
3		.10	.49	1186.60	630	320	305		71	110		3.9
4		.12	.59	1187.51	625	320	310		78	112		4.3
5		.10	.49	1188.37	630	290	310		86	118		4.0
6		.13	.64	1189.32	640	280	310		72	118		4.7
7		.11	.54	1190.20	645	320	320		70	118		4.1
8		.11	.54	1190.95	640	330	250		80	120		4.1
9	10:59	.02	.10	1191.36	620	280	280		92	125		2.0
10		.14	.69	1192.33	620	300	280		82	125		4.9
11		.14	.69	1193.32	640	320	320		72	124		5.7
12		.12	.59	1194.24	640	320	320		72	128		4.7
13		.02	.105	1194.69	630	310	320		85	130		2.3
14		.16	.82	1195.74	630	300	310		95	130		6.5
15	12:01	.15	.75	1196.77	655	285	300		95	130		6.7
16		.08	.40	1197.52	640	300	300		78	130		4.3
17		.14	.70	1198.50	640	290	300		88	130		6.0
18		.16	.80	1199.55	640	300	300		85	130		6.5
19	2min	.15	.75	1200.90	645	320	310		72	128		6.3
20		.08	.40	1201.65	640	220	305		70	130		4.3
21	12:34	.05	.25	1202.20	630	300	300		88	130		4.3
22		.16	.80	1203.30	640	310	310		80	130		7.0
23		.13	.65	1204.25	650	320	310		74	130		6.0
24		.12	.60	1205.132	650	320	310		73	131		5.5
Average		.115	.57		635.8							

Nomograph Setup

METER VOL. END 1205.12
START 1193.718
SAMPLE VOL. 21.414 ft³unc.

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
.837	23.79	23.82

Percent O₂ =

P_{meter} = C =
P_{stack} = T_{stack} =
T_{meter} = ΔP =
ΔH_g = Noz(Ideal) =
% H₂O = Noz(Actual) = .381

P = .37

Imp. Vol. (End) Vol. (Start) ΔVol. (ml)
#1 128 - 100 = 28
#2 105 - 100 = 5
#3 0 - 0 = 0
Total 33

#4 g(End) g(Start) Δgrams
Silica 1530 - 150.0 = 5
Gel
Total Vol. H₂O 32 ml

Corr. Vol. 23.311 ft³

78

PARTICULATE

DATA

Leak Check Rate

ISOKINETICS = 99

TEST NUMBER 37

Vac
in. Hg ft³/min

DATE 11-1-77

Sampling Time
Per Point, Min
1.5Before
After

OPERATOR RAP+DEC

FUEL Consolidation Coal

SITE A

PROBE LOCATION RLR OUT

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F							O ₂ , %	Vac.
		Δ P _s	Δ H	Meter Reading	Stack	Probe	Oven	Impingers		Meter			
								In	Out				
1	15:59	.08	.39	1211.30	640	290	275	?	105	130		3.2	
2		.17	.84	1212.39	650	320	280		95	130		6.0	
3		.12	.59	1213.28	660	320	290		90	130		4.5	
4		.11	.54	1214.14	660	330	290		88	130		4.2	
5		.02	.10	1214.54	640	320	320		90	130		2.0	
6		.17	.84	1215.62	645	300	310		90	130		6.2	
7		.15	.74	1216.63	660	320	315		82	130		5.4	
8		.09	.44	1217.40	670	330	330		80	130		4.0	
9		.02	.10	1217.80	645	320	300		88	132		—	
10		.18	.89	1218.89	650	290	310		88	132		6.5	
11		.18	.89	1219.95	670	300	320		80	135		6.6	
12		.11	.54	1220.82	680	330	315		70	135		4.5	
13	16:31	.05	.25	1221.40	630	280	300		80	135		—	
14		.18	.89	1222.48	650	280	310		80	136		6.7	
15		.17	.84	1223.54	650	280	310		75	138		6.3	
16		.13	.64	1224.46	650	310	310		72	139		5.0	
17		.16	.72	1225.50	—	300	320		80	140		5.2	
18	2min	.18	.89	1226.93	—	310	320		75	140		6.3	
19		.15	.74	1227.91	—	310	320		72	140		5.5	
20		.08	.39	1228.63	—	310	320		72	141		3.7	
21		.10	.49	1229.41	—	310	320		88	142		4.2	
22		.17	.84	1230.46	—	290	315		82	142		6.3	
23		.12	.59	1231.35	—	300	315		79	142		4.8	
24		.13	.64	1232.258	—	300	310		79	142		5.1	
Average													

Nomograph Setup

METER VOL. END 1222.85

START 1210.54

SAMPLE VOL 21.714 ft³ O₂

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
.93	23.60	23.64

Percent O₂ =

P_{meter} = C
 P_{stack} = T_{stack}
 T_{meter} = ΔP
 ΔH_g = Noz(Ideal) =
 % H₂O = Noz(Actual) = J #1
 T = 37

Imp.	Vol. (End)	Vol. (Start)	ΔVol. (ml)
#1	128	100	28
#2	105	100	5
#3	0	0	0
			Total 33
#4	g(End)	g(Start)	Δgrams
Silica Gel	1600	1500	10
			Total Vol. H ₂ O 43 ml

Corr. Vol = 23.638 ft³

PARTICULATE

DATA

Leak Check Rate

ISOKINETICS = 100%

TEST NUMBER 38

Vac
in. Hg ft³/min

DATE 11/2/77

OPERATOR RAP + JEC

FUEL Consolidation coal

SITE A

PROBE LOCATION BLR05

Sampling Time Per Point, Min
1.5

Before 150 0.02
After

* Nomograph Change

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F						O ₂ , %	Vac.
		ΔP _s	ΔH	Meter Reading	Stack	Probe	Oven	Impingers		Meter		
								In	Out			
1	11:12	.06	.30	1233.05	560	300	320	5	100	120		3.0
2		.08	.40	1233.84	600	310	320		92	120		3.5
3		.08	.40	1234.61	600	325	325		85	120		3.5
4		.07	.35	1235.32	570	325	325		83	122		3.2
5		.07	.35	1236.04	580	320	320		82	123		3.2
6		.09	.45	1236.85	600	300	315		80	124		3.6
7		.07	.35	1237.56	610	310	315		75	125		3.2
8		.04	.20	1238.11	570	320	320		75	125		2.5
9		.01	.05	1238.41	585	240	325		105	130		4.20
10		.07	.35	1239.12	590	290	320		90	130	*.36	3.2
11		.07	.36	1239.86	590	310	320		80	132		3.2
12		.05	.26	1240.47	590	315	315		74	132		2.8
13	11:52	.01	.05	1240.78	565	300	305		82	132		4.20
14		.09	.47	1241.58	585	290	310		82	132		4.0
15		.10	.52	1242.43	590	310	310		75	133		4.2
16		.05	.26	1243.02	560	325	330		70	133	*.35	2.8
17		.09	.48	1243.84	545	315	320		80	138		3.8
18		.10	.54	1244.72	585	320	325		72	138		4.3
19		.08	.43	1245.46	595	320	315		72	138		3.6
20		.05	.265	1246.06	—	320	315		72	139		2.8
21		.07	.37	1246.78	570	320	310		82	140		3.3
22		.10	.54	1247.64	580	310	310		80	140		—
23		.08	.43	1248.39	590	315	310		73	140		3.6
24		.07	.37	1249.082	570	315	315		72	142		3.3
Average												
		.068	.3565		582							

Nomograph Setup

METER VOL. END 1249.02
START 222.387

SAMPLE VOL. 16.69 ft³ STC

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
.837	23.68	23.71

Percent O₂ =

P_{meter} = C
P_{stack} = T_{stack}
T_{meter} = ΔP
ΔH_g = Noz (Ideal) =
% H₂O = Noz (Actual) = .38

Y = .3)

Imp. Vol. (End) Vol. (Start) ΔVol. (ml)
#1 121 - 100 = 21
#2 101 - 100 = 1
#3 0 - 0 = 0
Total 22

#4 g(End) g(Start) Δgrams
Silica 154.3 - 150 = 4.3
Gel
Total Vol. H₂O 263 ml

Corr. Vol. = 18.179 ft³

PARTICULATE

DATA

Leak Check Rate

ISOKINETICS - 101

TEST NUMBER 39

Vac
in. Hg ft³/min

DATE 11/2/77

Sampling Time
Per Point, Min
1.5Before 12.0 0.01
After

OPERATOR RAP

FUEL Consolidation

SITE A

PROBE LOCATION BLR. OUT.

Sample Point	Time	METER CONDITIONS			TEMPERATURES, °F						O ₂ , %	Vac.
		Δ P _s	Δ H	Meter Reading	Stack	Probe	Oven	Impingers		Meter		
								In	Out			
1		.05	.265	1250.27	565	300	315		112	130		2.7
2		.09	.47	1251.10	570	310	310		100	130		3.6
3	16:52	.07	.37	1251.83	580	320	300		90	130		3.0
4	16:52	.08	.43	1252.62	560	320	310		82	130		3.2
5		.07	.37	1253.33	550	290	320		90	135		3.0
6		.09	.47	1254.14	560	320	295		79	135		3.6
7		.09	.47	1254.95	570	320	245		79	135		3.6
8		.04	.21	1255.51	570	320	295		78	135		2.4
9		.01	.05	1255.79	560	310	295		92	138		2.0
10		.08	.43	1256.58	580	300	225		92	138		3.2
11		.08	.43	1257.34	585	320	280		80	138		3.5
12		.06	.32	1258.01	585	320	280		80	140		3.0
13		.01	.05	1258.30	565	300	245		92	142		2.0
14		.06	.32	1258.98	570	290	280		92	142		3.0
15		.07	.37	1259.71	585	310	285		85	142		3.2
16		.07	.37	1260.40	570	320	290		83	142		3.2
17		.09	.43	1261.19	570	260	290		112	145		3.5
18		.09	.48	1262.00	585	275	290		92	145		3.7
19		.08	.43	1262.77	570	290	290		85	145		3.5
20		.04	.21	1263.30	570	290	290		85	145		2.5
21		.07	.37	1264.01	570	290	290		95	145		3.2
22		.08	.43	1264.78	580	290	300		88	145		—
23		.06	.32	1265.44	585	310	290		83	145		3.1
24		.06	.32	1266.100	570	310	290		83	145		3.1
Average												

Nomograph Setup

METER VOL. END 1266.100

START 1249.640

SAMPLE VOL. 16.4% ft³/unc.

C _{pitot}	Stack Press. In. Hg-Gauge	Barometric Pressure
.837	23.68	23.71

Percent O₂ =

P_{meter} = C =
 P_{stack} = T_{stack} =
 T_{meter} = ΔP =
 ΔH_g = Noz(Ideal) =
 % H₂O = Noz(Actual) = .381

γ = .305

Imp.	Vol. (End)	Vol. (Start)	ΔVol. (ml)
#1	125	100	25
#2	1025	100	2.5
#3	0	0	0
			Total 27.5
#4	g(End)	g(Start)	Δgrams
Silica Gel	154.5	150.0	4.5
			Total Vol. H ₂ O 32 ml

Corr. Vol. = 17.918 ft³

PARTICULATE LAB WORKSHEET

TEST NO. 3 ^{mech. out} (~~Inlet, Outlet~~)

LOCATION ABMA SITE 4

Date 8/11/77

Box No. _____

Eng. RAP + JEC

Test Description _____

Dry Gas Meter Vol (ft³)

Final _____

Initial _____

Δ DgV _____

Final

Initial

Δ Vlc

Impinger Water Vol (ml)

1	2	3	Total
 	 	 	
 	 	 	
 	 	 	

CONTENT	H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.	
BOTTLE NO.	X			3	X	
BEAKER NO.		1	2			
DATE WT.		8/12/77	8/12/77	8/9/77		
TARE WT.						
1		69.5947	51.8184	.7459		
2		69.5943	51.8185	.7458		
3		69.5949	51.8184	.7456		
4						
AVG.		69.5946	51.8184	.7458		

POST TEST WTS.

1	X	69.7627	52.1981	.8819	X	
2		69.7627	52.1984	.8823		
3		69.7627	52.1984	.8819		
4						
AVG.		69.7627	52.1983	.8820		
Δ WT.		.1681	.3799	.1362		

Δ Vlc = _____ ml

LOAD _____ klb/hr

Δ DgV = _____ ft³

O₂ _____ %

Δ Mn 684.2 mgm

REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 4 ^{mech OUT} (~~Inlet, Outlet~~) LOCATION ABMA-site A
 Date 8/17/77 Box No. _____ Eng. RAF
 Test Description _____

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Impinger Water Vol (ml)

Final _____
 Initial _____
 Δ Vlc _____

1	2	3	Total

CONTENT	H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.
BOTTLE NO.				<u>4</u>	
BEAKER NO.		<u>3</u>	<u>4</u>	<u>—</u>	
DATE WT.		<u>8/19/77</u>	<u>8/19/77</u>	<u>8/12/77</u>	
TARE WT. 1		<u>69.0768</u>	<u>64.3992</u>	<u>.7579</u>	
2		<u>69.0366</u>	<u>64.3994</u>	<u>.7576</u>	
3		<u>69.0367</u>	<u>64.3994</u>	<u>.7576</u>	
4					
AVG.		<u>69.0367</u>	<u>64.3993</u>	<u>.7577</u>	

POST TEST WTS.

1		<u>69.1869</u>	<u>64.7910</u>	<u>.8672</u>	
2		<u>69.1870</u>	<u>64.7911</u>	<u>.8645</u>	
3		<u>69.1869</u>	<u>64.7913</u>	<u>.8654</u>	
4				<u>.8648</u>	
AVG.		<u>69.1869</u>	<u>64.7911</u>	<u>.8649</u>	
Δ WT.		<u>.1502</u>	<u>.8918</u>	<u>.1072</u>	

Δ Vlc = _____ ml LOAD _____ klb/hr
 Δ DgV = _____ ft³ O₂ _____ %
 Δ Mn 649.2 mgm REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 5 ^{mech. OUT.}
(~~Filtering Outlet~~)

LOCATION ABMA-SITE A

Date 8/18/77

Box No. _____

Eng. _____

Test Description _____

Dry Gas Meter Vol (ft³)

Final _____

Initial _____

Δ DgV _____

Final

Initial

Δ Vlc

Impinger Water Vol (ml)

1	2	3	Total
 	 	 	
 	 	 	
 	 	 	

CONTENT	H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.	
BOTTLE NO.	 			1	 	
BEAKER NO.		5	6	—		
DATE WT.		8/19/77	8/19/77	8/18/77		
TARE WT. 1		64.0685	69.0612	.7518		
2		64.0687	69.0614	.7516		
3		64.0685	69.0614	.7516		
4						
AVG.		64.0686	69.0613	.7517		

POST TEST WTS.

1	 	64.2877	69.4748	.9872	 	
2		64.2878	69.4749	.9872		
3		64.2877	69.4752	.9873		
4						
AVG.		64.2877	69.4749	.9872		
Δ WT.		.2191	.4136	.2335		

Δ Vlc = _____ ml

LOAD _____ klb/hr

Δ DgV = _____ ft³

O₂ _____ %

Δ Mn 866.2 mgm

REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 6 ^{mech. OUT} (~~Inlet, Outlet~~) LOCATION ABMA - SITE A
 Date 8/18/77 Box No. _____ Eng. _____
 Test Description _____

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Final _____
 Initial _____
 Δ Vlc _____

Impinger Water Vol (ml)

1	2	3	Total
 	 	 	
 	 	 	
 	 	 	

CONTENT	H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.
BOTTLE NO.	 	 	 	2	
BEAKER NO.	 	8	7	—	
DATE WT.	 	8/19/77	8/19/77	8/12/77	
TARE WT. 1	 	64.1195	50.3093	.7495	
2	 	64.1200	50.3092	.7494	
3	 	64.1200	50.3097	.7497	
4	 	 	 	 	
AVG.	 	64.1197	50.3096	.7495	

POST TEST WTS.

1	 	64.4392	50.9213	1.0276	
2	 	64.4395	50.9284	1.0266	
3	 	64.4396	50.9288	1.0264	
4	 	 	 	 	
AVG.	 	64.4394	50.9285	1.0269	
Δ WT.	 	.3197	.6185	.2774	

Δ Vlc = _____ ml
 Δ DgV = _____ ft³
 Δ Mn 1216.0 mgm

LOAD _____ klb/hr
 O₂ _____ %

REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 10 ^{mech. out} (~~Enviro, dust~~) LOCATION ABMA - SITE A
 Date 8/24/77 Box No. _____ Eng. _____
 Test Description _____

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Impinger Water Vol (ml)

Final _____
 Initial _____
 Δ Vlc _____

1	2	3	Total
 	 	 	
 	 	 	
 	 	 	

CONTENT	H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.	
BOTTLE NO.	 	—	—	6	 	
BEAKER NO.	 	10	9	—	 	
DATE WT.	 	8/25/77	8/25/77	—	 	
TARE WT. 1	 	69.5976	64.0683	.7553	 	
2	 	69.5976	64.0682	.7554	 	
3	 	69.5978	64.0680	.7554	 	
4	 	—	—	—	 	
AVG.	 	69.5976	64.0681	.7554	 	

POST TEST WTS.

1	 	69.7912	64.3051	.8571	 	
2	 	69.7224	64.3051	Extremely	 	
3	 		64.3052	Hygroscopic	 	
4	 	69.7496	—		 	
AVG.	 		64.3051	.8571	 	
Δ WT.	 		0.2370	.1017	 	

Δ Vlc = _____ ml
 Δ DgV = _____ ft³
 Δ Mn _____ mgm

LOAD _____ klb/hr
 O₂ _____ %
 REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 14 ^{Mech. Out} (~~Inlet, Outlet~~) LOCATION ABMA - SITE A
 Date 8/26/77 Box No. _____ Eng. _____
 Test Description _____

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Final _____
 Initial _____
 Δ Vlc _____

Impinger Water Vol (ml)			
1	2	3	Total
 	 	 	
 	 	 	
 	 	 	

CONTENT	H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.	
BOTTLE NO.	 	—	—	—	 	
BEAKER NO.	 	11	—	7	 	
DATE WT.	 	8/29/77	—	—	 	
TARE WT.	1	69.0363	—	.7620	 	
	2	69.0364	—	.7619	 	
	3	69.0364	—	.7620	 	
	4	—	—	—	 	
AVG.	 	69.0364	—	.7620	 	

POST TEST WTS.

1	 	69.6576	—	.9367	 	
2	 	69.6579	—	.9638	 	
3	 	69.6580	—	.9638	 	
4	 	—	—	—	 	
AVG.	 	69.6578	—	.9638	 	
Δ WT.	 	.6214	—	.2018	 	

Δ Vlc = _____ ml

LOAD _____ klb/hr

Δ DgV = _____ ft³

O₂ _____ %

Δ Mn 823.2 mgm

REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 15 ^{mech. OUT} (~~Inlet, Outlet~~) LOCATION ABMA - Site A
 Date 7/22/77 Box No. _____ Eng. _____
 Test Description _____

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Impinger Water Vol (ml)

Final _____
 Initial _____
 Δ Vlc _____

1	2	3	Total

CONTENT	H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.	
BOTTLE NO.		—	—	8		
BEAKER NO.		12	13	—		
DATE WT.		8/29/77	8/29/77	—		
TARE WT.	1	64.1199	51.8218	.7649		
	2	64.1200	51.8220	.7649		
	3	64.1201	51.8220	.7648		
	4	—	—	—		
AVG.		64.1200	51.8219	.7649		

POST TEST WTS.

	1	64.3580	52.1146	.9504		
	2	64.3581	52.1146	.9507		
	3	64.3582	52.1147	.9507		
	4	—	—	—		
AVG.		64.3581	52.1146	.9506		
Δ WT.		.2381	.2927	.1857		

Δ Vlc = _____ ml
 Δ DgV = _____ ft³
 Δ Mn 716.5 mgm

LOAD _____ klb/hr
 O₂ _____ %

REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 16A ^{Mech. OUT} (~~Inlet, Outlet~~) LOCATION ABMA - SITE 4
 Date 8/30/77 Box No. _____ Eng. _____
 Test Description _____

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Final _____
 Initial _____
 Δ Vlc _____

Impinger Water Vol (ml)			
1	2	3	Total
 	 	 	
 	 	 	
 	 	 	

CONTENT		H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.	
BOTTLE NO.		 	<u>1</u>	<u>—</u>	<u>—</u>	 	
BEAKER NO.		 	<u>17</u>	<u>16</u>	<u>9</u>	 	
DATE WT.		 	<u>9/1/77</u>	<u>9/1/77</u>	<u>—</u>	 	
TARE WT.	1	 	<u>64.3992</u>	<u>50.3092</u>	<u>.7520</u>	 	
	2	 	<u>64.3986</u>	<u>50.3093</u>	<u>.7518</u>	 	
	3	 	<u>64.3989</u>	<u>50.3095</u>	<u>.7517</u>	 	
	4	 	<u>—</u>	<u>—</u>	<u>—</u>	 	
AVG.		 	<u>64.3989</u>	<u>50.3095</u>	<u>.7518</u>	 	

POST TEST WTS.

	1	 	<u>64.6006</u>	<u>50.4938</u>	<u>.8841</u>	 	
	2	 	<u>64.6002</u>	<u>50.4936</u>	<u>.8842</u>	 	
	3	 	<u>64.6000</u>	<u>50.4937</u>	<u>.8846</u>	 	
	4	 	<u>—</u>	<u>—</u>	<u>—</u>	 	
AVG.		 	<u>64.6003</u>	<u>50.4937</u>	<u>.8843</u>	 	
Δ WT.		 	<u>.2014</u>	<u>.1842</u>	<u>.1325</u>	 	

Δ Vlc = _____ ml
 Δ DgV = _____ ft³
 Δ Mn 518.1 mgm

LOAD _____ klb/hr
 O₂ _____ %
 REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 16B ^{ESP OUT} (~~Inlet, Outlet~~) LOCATION ABMA - Site A
 Date 8/30/77 Box No. _____ Eng. _____
 Test Description _____

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Impinger Water Vol (ml)

Final _____
 Initial _____
 Δ Vlc _____

1	2	3	Total
 	 	 	
 	 	 	
 	 	 	

CONTENT	H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.	
BOTTLE NO.	 	<u>2</u>	 	<u>—</u>	 	
BEAKER NO.	 	<u>18</u>	 	<u>10</u>	 	
DATE WT.	 	<u>9-1-77</u>	 	<u>—</u>	 	
TARE WT. 1	 	<u>69.0615</u>	 	<u>.7537</u>	 	
2	 	<u>69.0608</u>	 	<u>.7537</u>	 	
3	 	<u>69.0610</u>	 	<u>.7537</u>	 	
4	 	<u>—</u>	 	<u>—</u>	 	
AVG.	 	<u>69.0611</u>	 	<u>.7537</u>	 	

POST TEST WTS.

1	 	<u>69.0715</u>	 	<u>.7814</u>	 	
2	 	<u>69.0716</u>	 	<u>.7810</u>	 	
3	 	<u>69.0714</u>	 	<u>.7813</u>	 	
4	 	<u>—</u>	 	<u>—</u>	 	
AVG.	 	<u>69.0715</u>	 	<u>.7812</u>	 	
Δ WT.	 	<u>.0104</u>	 	<u>.0275</u>	 	

Δ Vlc = _____ ml
 Δ DgV = _____ ft³
 Δ Mn 37.9 mgm

LOAD _____ klb/hr
 O₂ _____ %

REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 17A ESP OUT (Inlet, Outlet) LOCATION ABMA-SITE A
 Date 8/31/77 Box No. _____ Eng. _____
 Test Description _____

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Final _____
 Initial _____
 Δ Vlc _____

Impinger Water Vol (ml)			
1	2	3	Total

CONTENT		H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.
BOTTLE NO.			3		—	
BEAKER NO.			15		11	
DATE WT.			9-1-77			
TARE WT.	1		64.0682		.7499	
	2		64.0681		.7498	
	3		64.0675		.7498	
	4		—		—	
AVG.			64.0679		.7498	

POST TEST WTS.

	1		64.0795		.7647	
	2		64.0791		.7649	
	3		64.0791		.7650	
	4		—		—	
AVG.			64.0792		.7649	
Δ WT.			.0113		.0151	

Δ Vlc = _____ ml
 Δ DgV = _____ ft³
 Δ Mn 26.4 mgm

LOAD _____ klb/hr
 O₂ _____ %

REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 17B STACK LOCATION ABMA-SITE A
 Date 8/31/77 Box No. _____ Eng. _____
 Test Description _____

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Impinger Water Vol (ml)

Final _____
 Initial _____
 Δ Vlc _____

1	2	3	Total
 	 	 	
 	 	 	
 	 	 	

CONTENT	H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.	
BOTTLE NO.	 	<u>4</u>	 	<u>—</u>	 	
BEAKER NO.	 	<u>14</u>	 	<u>5</u>	 	
DATE WT.	 	<u>9/1/77</u>	 	 	 	
TARE WT.	1	<u>69.0366</u>	 	<u>.7540</u>	 	
	2	<u>69.0360</u>	 	<u>.7537</u>	 	
	3	<u>69.0361</u>	 	<u>.7538</u>	 	
	4	<u>—</u>	 	<u>—</u>	 	
AVG.		<u>69.0362</u>	 	<u>.7538</u>	 	

POST TEST WTS.

	1	<u>69.0474</u>	 	<u>.7661</u>	 	
	2	<u>69.0469</u>	 	<u>.7661</u>	 	
	3	<u>69.0468</u>	 	<u>.7656</u>	 	
	4	<u>—</u>	 	<u>—</u>	 	
AVG.		<u>69.0470</u>	 	<u>.7659</u>	 	
Δ WT.		<u>.0108</u>	 	<u>.0121</u>	 	

Δ Vlc = _____ ml
 Δ DgV = _____ ft³
 Δ Mn 22.9 mgm

LOAD _____ klb/hr
 O₂ _____ %

REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 21 ^{BLR OUT} (~~Wet, Subst~~) LOCATION ABMA SITE A
 Date 9/23/77 Box No. _____ Eng. _____
 Test Description _____

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Final _____
 Initial _____
 Δ Vlc _____

Impinger Water Vol (ml)			
1	2	3	Total
 	 	 	
 	 	 	
 	 	 	

CONTENT	H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.	
BOTTLE NO.	 	—	—	—	 	
BEAKER NO.	 	21	19	14	 	
DATE WT.	 	9/25/77	9/25/77	9/10/77	 	
TARE WT.	1	64.1198	64.3976	.7584	 	
	2	64.1200	64.3976	.7584	 	
	3	64.1199	64.3975	.7584	 	
	4	—	—	—	 	
AVG.	 	64.1199	64.3976	.7584	 	

POST TEST WTS.

1	 	64.3764	73.9676	.8944	 	
2	 	64.3762	73.9681	.8946	 	
3	 	64.3765	73.9678	.8946	 	
4	 	—	—	—	 	
AVG.	 	64.3764	73.9678	.8945	 	
Δ WT.	 	.2565	9.5702	.1361	 	

Δ Vlc = _____ ml
 Δ DgV = _____ ft³
 Δ Mn 9962.8 mgm

LOAD _____ klb/hr
 O₂ _____ %

REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 22 ^{BLR OUT} (~~Inlet, Outlet~~) LOCATION ABMA - SITE A
 Date 9/23/77 Box No. _____ Eng. _____
 Test Description _____

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Final _____
 Initial _____
 Δ Vlc _____

Impinger Water Vol (ml)

1	2	3	Total
 	 	 	
 	 	 	
 	 	 	

CONTENT	H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.	
BOTTLE NO.	 	 	 	 	 	
BEAKER NO.	 	<u>26</u>	<u>20</u>	<u>15</u>	 	
DATE WT.	 	<u>9/25/77</u>	<u>9/25/77</u>	<u>9/10/77</u>	 	
TARE WT. 1	 	<u>64.0683</u>	<u>50.3089</u>	<u>.7557</u>	 	
2	 	<u>64.0683</u>	<u>50.3091</u>	<u>.7557</u>	 	
3	 	<u>64.0681</u>	<u>50.3090</u>	<u>.7557</u>	 	
4	 	<u> </u>	<u> </u>	<u> </u>	 	
AVG.	 	<u>64.0682</u>	<u>50.3090</u>	<u>.7557</u>	 	

POST TEST WTS.

1	 	<u>64.2755</u>	<u>65.6109</u>	<u>1.0070</u>	 	
2	 	<u>64.2752</u>	<u>65.6112</u>	<u>1.0072</u>	 	
3	 	<u>64.2753</u>	<u>65.6113</u>	<u>1.0072</u>	 	
4	 	<u> </u>	<u> </u>	<u> </u>	 	
AVG.	 	<u>64.2753</u>	<u>65.6111</u>	<u>1.0071</u>	 	
Δ WT.	 	<u>.2071</u>	<u>15.3021</u>	<u>.2514</u>	 	

Δ Vlc = _____ ml
 Δ DgV = _____ ft³
 Δ Mn 15,760.6 mgm

LOAD _____ klb/hr

O₂ _____ %

REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 23 ^{BLROUT} (~~Inlet~~, ~~Outlet~~) LOCATION ABMA-SITE A
 Date 9/24/77 Box No. _____ Eng. _____
 Test Description _____

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Impinger Water Vol (ml)

Final _____
 Initial _____
 Δ Vlc _____

1	2	3	Total
 	 	 	
 	 	 	
 	 	 	

CONTENT	H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.	
BOTTLE NO.	 				 	
BEAKER NO.		23	22	16		
DATE WT.		9/25/77	9/25/77	9/10/77		
TARE WT. 1		69.5973	51.8214	.7576		
2		69.5973	51.8217	.7574		
3		69.5972	51.8218	.7574		
4		—	—	—		
AVG.		69.5973	51.8216	.7575		

POST TEST WTS.

1	 	69.7121	57.5637	.8622	 	
2		69.7123	57.5641	.8617		
3		69.7124	57.5638	.8620		
4		—	—	—		
AVG.		69.7123	57.5639	.8620		
Δ WT.		.1150	5.7423	.1045		

Δ Vlc = _____ ml
 Δ DgV = _____ ft³
 Δ Mn 5961.8 mgm

LOAD _____ klb/hr
 O₂ _____ %

REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 24 ^{BLR OUT} (~~Inlet~~, ~~Outlet~~) LOCATION ABMA - SITE A
 Date 9/24/77 Box No. _____ Eng. _____
 Test Description _____

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Final _____
 Initial _____
 Δ Vlc _____

Impinger Water Vol (ml)

1	2	3	Total

CONTENT	H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.
BOTTLE NO.					
BEAKER NO.		<u>24</u>	<u>25</u>	<u>17</u>	
DATE WT.		<u>9/25/77</u>	<u>9/25/77</u>	<u>9/10/77</u>	
TARE WT.	1	<u>69.0357</u>	<u>69.0611</u>	<u>.7431</u>	
	2	<u>69.0356</u>	<u>69.0608</u>	<u>.7429</u>	
	3	<u>69.0358</u>	<u>69.0611</u>	<u>.7429</u>	
	4	<u>—</u>	<u>—</u>	<u>—</u>	
AVG.		<u>69.0357</u>	<u>69.0610</u>	<u>.7430</u>	

POST TEST WTS.

1		<u>69.1762</u>	<u>73.5375</u>	<u>.8449</u>	
2		<u>69.1767</u>	<u>73.5375</u>	<u>.8447</u>	
3		<u>69.1765</u>	<u>73.5376</u>	<u>.8447</u>	
4		<u>—</u>	<u>—</u>	<u>—</u>	
AVG.		<u>69.1765</u>	<u>73.5375</u>	<u>.8448</u>	
Δ WT.		<u>.1408</u>	<u>4.4765</u>	<u>.1018</u>	

Δ Vlc = _____ ml

LOAD _____ klb/hr

Δ DgV = _____ ft³

O₂ _____ %

Δ Mn 4719.1 mgm

REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 26A Boiler Outlet
(Inlet, ~~Outlet~~) LOCATION ABMA-SITE A
 Date 10/1/77 Box No. _____ Eng. _____
 Test Description BLR OUT

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Final _____
 Initial _____
 Δ Vlc _____

Impinger Water Vol (ml)			
1	2	3	Total
_____	_____	_____	_____
_____	_____	_____	_____
_____	_____	_____	_____

CONTENT		H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.	
BOTTLE NO.		X				X	
BEAKER NO.			21	20	18		
DATE WT.			10-11-77	10/11/77	—		
TARE WT.	1		64.1201	50.3095	.7709		
	2		64.1199	50.3094	.7708		
	3		64.1197	50.3095	.7708		
	4		—	—			
AVG.			64.1199	50.3095	.7708		

POST TEST WTS.

1	X	<u>64.2592</u>	<u>56.4736</u>	<u>.8603</u>	X
2		<u>64.2601</u>	<u>extremely</u>	<u>.8601</u>	
3		<u>—</u>	<u>Hygroscopic</u>	<u>.8603</u>	
4		<u>—</u>			
AVG.		<u>64.2596</u>	<u>56.4736</u>	<u>.8603</u>	
Δ WT.		<u>0.1398</u>	<u>6.1641</u>	<u>.0894</u>	

Δ Vlc = _____ ml

LOAD _____ klb/hr

Δ DgV = _____ ft³

O₂ _____ %

Δ Mn 6393.7 mgm

REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 26B ^{Mech. OUT}
 (Inlet, ~~Outlet~~) LOCATION ABMA SITE A
 Date 10/11/77 Box No. _____ Eng. _____
 Test Description _____

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Final _____
 Initial _____
 Δ Vlc _____

Impinger Water Vol (ml)

1	2	3	Total
 	 	 	
 	 	 	
 	 	 	

CONTENT	H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.	
BOTTLE NO.	 	 	 	 	 	
BEAKER NO.	 	<u>16</u>	<u>22</u>	<u>19</u>	 	
DATE WT.	 	<u>10/11/77</u>	<u>10/11/77</u>	<u>10/10/77</u>	 	
TARE WT.	1	<u>69.5970</u>	<u>51.8218</u>	<u>.7762</u>	 	
	2	<u>69.5973</u>	<u>51.8218</u>	<u>.7762</u>	 	
	3	<u>69.5972</u>	<u>51.8217</u>	<u>.7762</u>	 	
	4	 	 	 	 	
AVG.	 	<u>69.5972</u>	<u>51.8218</u>	<u>.7762</u>	 	

POST TEST WTS.

1	 	<u>69.7721</u>	<u>52.2484</u>	<u>1.0144</u>	 	
2	 	<u>69.7726</u>	<u>52.2488</u>	<u>1.0145</u>	 	
3	 	<u>—</u>	<u>—</u>	<u>1.0147</u>	 	
4	 	<u>—</u>	<u>—</u>	 	 	
AVG.	 	<u>69.7724</u>	<u>52.2486</u>	<u>1.0145</u>	 	
Δ WT.	 	<u>0.1752</u>	<u>0.4268</u>	<u>0.2383</u>	 	

Δ Vlc = _____ ml
 Δ DgV = _____ ft³
 Δ Mn 840.3 mgm

LOAD _____ klb/hr

O₂ _____ %

REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 28 Boiler Outlet
(Inlet, Outlet) LOCATION ABMA- SITE A
 Date 10/11/77 Box No. _____ Eng. _____
 Test Description _____

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Final _____
 Initial _____
 Δ Vlc _____

Impinger Water Vol (ml)			
1	2	3	Total
 	 	 	
 	 	 	
 	 	 	

CONTENT	H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.	
BOTTLE NO.	X					X
BEAKER NO.		17	23	21		
DATE WT.		10/11/77	10/11/77			
TARE WT.						
1		69.0598	69.0355	.7581		
2		69.0600	69.0355	.7581		
3		69.0603	—	.7582		
4		—	—	—		
AVG.		69.0601	69.0355	.7581		

POST TEST WTS.

1	X	69.3755	84.8521	.8892	X
2		69.3759	84.8526	.8896	
3		—	—	.8898	
4		—	—	—	
AVG.		69.3757	84.8524	.8895	
Δ WT.		0.3156	15.8168	.1314	

Δ Vlc = _____ ml
 Δ DgV = _____ ft³
 Δ Mn 16,263.9 mgm

LOAD _____ klb/hr
 O₂ _____ %
 REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 29 ^{BLR OUT} (~~Inlet~~, Outlet) LOCATION ABMA - SITE A
 Date 10/11/77 Box No. _____ Eng. _____
 Test Description _____

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Final _____
 Initial _____
 Δ Vlc _____

Impinger Water Vol (ml)

1	2	3	Total
 	 	 	
 	 	 	
 	 	 	

CONTENT	H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.	
BOTTLE NO.	 	 	 	 	 	
BEAKER NO.	 	<u>19</u>	<u>26</u>	<u>22</u>	 	
DATE WT.	 	<u>10/11/77</u>	<u>10/11/77</u>	<u>10/10/77</u>	 	
TARE WT.	1	<u>64.3976</u>	<u>64.0673</u>	<u>.7583</u>	 	
	2	<u>64.3978</u>	<u>64.0672</u>	<u>.7583</u>	 	
	3	<u>64.3978</u>	<u>64.0671</u>	<u>.7583</u>	 	
	4	<u>—</u>	<u>—</u>	<u>—</u>	 	
AVG.		<u>64.3977</u>	<u>64.0672</u>	<u>.7583</u>	 	

POST TEST WTS.

1	 	<u>64.6192</u>	<u>75.8618</u>	<u>.8915</u>	 	
2	 	<u>64.6196</u>	<u>75.8630</u>	<u>.8917</u>	 	
3	 	<u>—</u>	<u>Hygroscopic</u>	<u>.8919</u>	 	
4	 	<u>—</u>	<u>—</u>	<u>—</u>	 	
AVG.		<u>64.6194</u>	<u>75.8624</u>	<u>.8917</u>	 	
Δ WT.		<u>0.2217</u>	<u>11.7952</u>	<u>0.1334</u>	 	

Δ Vlc = _____ ml

LOAD _____ klb/hr

Δ DgV = _____ ft³

O₂ _____ %

Δ Mn 12,150.3 mgm

REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 34A BLR OUT (Inlet, Outlet) LOCATION ABMA - SITE A
 Date 10/27/77 Box No. _____ Eng. _____
 Test Description _____

Dry Gas Meter Vol (ft³)
 Final _____
 Initial _____
 Δ DgV _____

Impinger Water Vol (ml)

1	2	3	Total
Final			
Initial			
Δ Vlc			

CONTENT		H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.	
BOTTLE NO.					18		
BEAKER NO.			17	37		21	
DATE WT.			—	—	10/26/77	—	
TARE WT.	1		69.0615	49.6490	.7414	64.1202	
	2		69.0613	49.6488	.7416	64.1205	
	3		69.0612	49.6488	.7412	64.1201	
	4		—	—	—	—	
AVG.			69.0613	49.6489	.7414	64.1202	

POST TEST WTS.

1		69.3196	64.6347	.8340	64.1257	
2		69.3199	64.6350	.8341	64.1265	
3		69.3199	64.6349	.8340	64.1268	
4		—	—	—		
AVG.		69.3198	64.6349	.8340	64.1263	
Δ WT.		.2585	14.9860	.0926	.0061	

Δ Vlc = _____ ml LOAD _____ klb/hr
 Δ DgV = _____ ft³ O₂ _____ %
 Δ Mn 15337.1 mgm REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 34 B ^{ESP OUT}
~~(Inlet, Outlet)~~

LOCATION ABMA - SITE A

Date 10/27/77

Box No. _____

Eng. _____

Test Description _____

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Final _____
 Initial _____
 Δ Vlc _____

Impinger Water Vol (ml)

1	2	3	Total
 	 	 	
 	 	 	
 	 	 	

CONTENT	H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.	
BOTTLE NO.	 	 	 	<u>19</u>	 	
BEAKER NO.	 	<u># 23</u>	 	<u>—</u>	 	
DATE WT.	 	 	 	<u>10-126177</u>	 	
TARE WT.	1	<u>69.0361</u>	 	<u>.7562</u>	 	
	2	<u>69.0363</u>	 	<u>.7565</u>	 	
	3	<u>69.0361</u>	 	<u>.7560</u>	 	
	4	<u>—</u>	 	<u>—</u>	 	
AVG.	 	<u>69.0362</u>	 	<u>.7562</u>	 	

POST TEST WTS.

	1	<u>69.0664</u>	 	<u>.8283</u>	 	
	2	<u>69.0666</u>	 	<u>.8283</u>	 	
	3	<u>69.0670</u>	 	<u>.8283</u>	 	
	4	<u>—</u>	 	<u>—</u>	 	
AVG.	 	<u>69.0667</u>	 	<u>.8283</u>	 	
Δ WT.	 	<u>.0305</u>	 	<u>.0721</u>	 	

Δ Vlc = _____ ml

LOAD _____ klb/hr

Δ DgV = _____ ft³

O₂ _____ %

Δ Mn 102.6 mgm

REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 35A DIR OUT
(~~Inlet~~, ~~Outlet~~) LOCATION ABMA SITE - A
 Date 10/30/77 Box No. _____ Eng. _____
 Test Description _____

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Final _____
 Initial _____
 Δ Vlc _____

Impinger Water Vol (ml)			
1	2	3	Total
 	 	 	
 	 	 	
 	 	 	

CONTENT		H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.	
BOTTLE NO.		 					
BEAKER NO.		 	<u>16</u>	<u>28</u>	<u>21</u>		
DATE WT.		 					
TARE WT.	1	 	<u>69.5974</u>	<u>50.4534</u>	<u>.7530</u>		
	2	 	<u>69.5973</u>	<u>50.4538</u>	<u>.7530</u>		
	3	 	<u>69.5973</u>	<u>50.4533</u>	<u>.7529</u>		
	4	 					
AVG.		 	<u>69.5973</u>	<u>50.4535</u>	<u>.7530</u>		

POST TEST WTS.

	1	 	<u>69.8518</u>	<u>78.0646</u>	<u>1.0591</u>		
	2	 	<u>69.8521</u>	<u>78.0657</u>	<u>1.0590</u>		
	3	 	<u>69.8520</u>	<u>78.0660</u>	<u>1.0589</u>		
	4	 					
AVG.		 	<u>69.8520</u>	<u>78.0654</u>	<u>1.0590</u>		
Δ WT.		 	<u>.2530</u>	<u>27.6119</u>	<u>3.060</u>		

Δ Vlc = _____ ml
 Δ DgV = _____ ft³
 Δ Mn 28,172.9 mgm

LOAD _____ klb/hr
 O₂ _____ %
 REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 35B ^{ESR OUT} (~~Inlet, Outlet~~) LOCATION ABMA - SITE A
 Date 10/30/71 Box No. _____ Eng. _____
 Test Description _____

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Impinger Water Vol (ml)

Final _____
 Initial _____
 Δ Vlc _____

1	2	3	Total

CONTENT	H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.	
BOTTLE NO.						
BEAKER NO.		19		22		
DATE WT.						
TARE WT.	1	64.3982		.7494		
	2	64.3985		.7493		
	3	64.3984		.7491		
	4					
AVG.		64.3984		.7493		

POST TEST WTS.

	1	64.4177		.7884		
	2	64.4181		.7885		
	3	64.4179		.7884		
	4					
AVG.		64.4179		.7884		
Δ WT.		.0195		.0391		

Δ Vlc = _____ ml
 Δ DgV = _____ ft³
 Δ Mn 58.6 mgm

LOAD _____ klb/hr
 O₂ _____ %

REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 36 *PLR OUT* (Inlet, ~~Outlet~~) LOCATION ABMA - SITE A
 Date 11/1/77 Box No. _____ Eng. _____
 Test Description _____

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Final _____
 Initial _____
 Δ Vlc _____

Impinger Water Vol (ml)

1	2	3	Total
 	 	 	
 	 	 	
 	 	 	

CONTENT	H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.	
BOTTLE NO.	 	36		23	 	
BEAKER NO.	 	32	31	—	 	
DATE WT.	 	11/3/77	—	—	 	
TARE WT. 1	 	68.4710	50.3086	.7545	 	
2	 	68.4706	50.3089	.7546	 	
3	 	68.4706	50.3084	.7546	 	
4	 	—	—	—	 	
AVG.	 	68.4707	50.3086	.7546	 	

POST TEST WTS.

1	 	68.6525	62.2552	.9466	 	
2	 	68.6528	62.2555	.9466	 	
3	 	68.6529	62.2557	.9467	 	
4	 	—	—	—	 	
AVG.	 	68.6527	62.2555	.9466	 	
Δ WT.	 	.1820	119.469	.1920	 	

Δ Vlc = _____ ml
 Δ DgV = _____ ft³
 Δ Mn 12,320.9 mgm

LOAD _____ klb/hr
 O₂ _____ %

REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 37 BLR OUT (Inlet, Outlet) LOCATION ABMA - SITE A
 Date 11/1/77 Box No. _____ Eng. _____
 Test Description _____

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Final _____
 Initial _____
 Δ Vlc _____

Impinger Water Vol (ml)

1	2	3	Total
 	 	 	
 	 	 	
 	 	 	

CONTENT	H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.	
BOTTLE NO.	 	<u>37</u>	 	<u>24</u>	 	
BEAKER NO.	 	<u>33</u>	<u>22</u>	<u>—</u>	 	
DATE WT.	 	<u>11/3/77</u>	<u>—</u>	<u>—</u>	 	
TARE WT. 1	 	<u>63.5574</u>	<u>51.8235</u>	<u>.7420</u>	 	
2	 	<u>63.5574</u>	<u>51.8222</u>	<u>.7420</u>	 	
3	 	<u>63.5572</u>	<u>51.8225</u>	<u>.7419</u>	 	
4	 	<u>—</u>	<u>—</u>	<u>—</u>	 	
AVG.	 	<u>63.5573</u>	<u>51.8229</u>	<u>.7420</u>	 	

POST TEST WTS.

1	 	<u>63.9039</u>	<u>66.0558</u>	<u>.8968</u>	 	
2	 	<u>63.9040</u>	<u>66.0559</u>	<u>.8966</u>	 	
3	 	<u>63.9042</u>	<u>66.0561</u>	<u>.8966</u>	 	
4	 	<u>—</u>	<u>—</u>	<u>—</u>	 	
AVG.	 	<u>63.9040</u>	<u>66.0559</u>	<u>.8967</u>	 	
Δ WT.	 	<u>.3467</u>	<u>14.2330</u>	<u>.1547</u>	 	

Δ Vlc = _____ ml
 Δ DgV = _____ ft³
 Δ Mn 14,234.4 mgm

LOAD _____ klb/hr
 O₂ _____ %

REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 38 (~~3122, 3123~~) ^{BLR OUT} LOCATION ABMA - SITE
 Date 11/2/77 Box No. _____ Eng. _____
 Test Description _____

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Final _____
 Initial _____
 Δ Vlc _____

Impinger Water Vol (ml)			
1	2	3	Total

CONTENT		H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.
BOTTLE NO.					25	
BEAKER NO.			36	37	—	
DATE WT.			11/3/77	11/3/77	—	
TARE WT.	1		64.1640	64.4221	.7335	
	2		64.1640	64.4220	.7334	
	3		64.1639	64.4221	.7332	
	4		—	—	—	
AVG.			64.1640	64.4221	.7334	

POST TEST WTS.

1		64.4567	67.3119	.7972	
2		64.4570	67.3123	.7969	
3		64.4571	67.3125	.7969	
4		—	—	—	
AVG.		64.4569	67.3122	.7970	
Δ WT.		.2929	2.8901	.0636	

Δ Vlc = _____ ml
 Δ DgV = _____ ft³
 Δ Mn 3246.6 mgm

LOAD _____ klb/hr
 O₂ _____ %

REMARKS: _____

PARTICULATE LAB WORKSHEET

TEST NO. 39 ~~(11/2/77)~~ ^{DLR OUT} LOCATION ABMA - SITE A
 Date 11/2/77 Box No. _____ Eng. _____
 Test Description min. O₂ FA.

Dry Gas Meter Vol (ft³)

Final _____
 Initial _____
 Δ DgV _____

Final _____
 Initial _____
 Δ Vlc _____

Impinger Water Vol (ml)

1	2	3	Total
 	 	 	
 	 	 	
 	 	 	

CONTENT	H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.	
BOTTLE NO.	 	<u>39</u>	<u>—</u>	<u>26</u>	 	
BEAKER NO.	 	<u>34</u>	<u>35</u>	<u>—</u>	 	
DATE WT.	 	<u>11/3/77</u>	<u>11/3/77</u>	<u>—</u>	 	
TARE WT.	1	<u>64.0685</u>	<u>69.5678</u>	<u>.7368</u>	 	
	2	<u>64.0683</u>	<u>69.5675</u>	<u>.7365</u>	 	
	3	<u>64.0682</u>	<u>69.5675</u>	<u>.7365</u>	 	
	4	<u>—</u>	<u>—</u>	<u>—</u>	 	
AVG.	 	<u>64.0683</u>	<u>69.5676</u>	<u>.7366</u>	 	

POST TEST WTS.

1	 	<u>64.3370</u>	<u>75.8657</u>	<u>.8354</u>	 	
2	 	<u>64.3373</u>	<u>75.8657</u>	<u>.8352</u>	 	
3	 	<u>64.3373</u>	<u>75.8658</u>	<u>.8353</u>	 	
4	 	<u>—</u>	<u>—</u>	<u>—</u>	 	
AVG.	 	<u>64.3372</u>	<u>75.8657</u>	<u>.8353</u>	 	
Δ WT.	 	<u>.2689</u>	<u>6.2981</u>	<u>.0987</u>	 	

Δ Vlc = _____ ml
 Δ DgV = _____ ft³
 Δ Mn 6,665.7 mgm

LOAD _____ klb/hr
 O₂ _____ %

REMARKS: _____

SECTION 3.0

GASEOUS DATA

	<u>PAGE</u>
3.1 GASEOUS EMISSION SUMMARY	110
3.2 GASEOUS EMISSION DATA SHEET	116
3.3 SO _x DATA SUMMARY	155
3.4 SO _x DATA SHEET	158

GASEOUS EMISSION SUMMARY

Location: A

Fuel: _____

TEST NO.	DATE	LOAD %	CONDITIONS	MULTICLONE OUTLET						ECON. OUTLET				SO ₂ ppm Dry	SO ₃ ppm Dry	NOTES
				O ₂ % Dry	CO ₂ % Dry	CO ppm Dry	NO ppm Dry	NO ₂ ppm Wet	HC ppm Wet	O ₂ % Dry	CO ₂ % Dry	CO ppm Dry	NO ppm Dry			
1	9 Aug 77	64	As Found	4.9	15.2	180	343			7.8	12.0	167	410	768	2	SO _x Mech. outlet
2A	10 Aug 77	59	As Found	4.3	16.0	86	345			5.6	14.2	175	380			Gaseous only
2B			reduce grate air	3.6	16.8	126	316									
2C			reduce grate air	2.7	17.9	266	285									
2D			reduce grate air	1.7	18.9	1072	256									
2E			raise grate air	3.7	16.8	127	302									
2F			raise grate air	4.4	15.7	174	325									
2G			raise grate air	5.1	14.8	91	358									
2H			raise grate air	5.9	13.6	95	400									
3	11 Aug 77	61	low grate air	4.1	16.9	219	312			5.9	13.9	203	340			Part. Mech. outlet
4A	17 Aug 77	60	high grate air	6.3	13.6	77	497			7.7	11.6	68	515			Part. Mech. outlet
4B				7.0												Brink Mech. outlet
5	18 Aug 77	72	low grate air	4.1	16.4	536	385			6.0	13.9	360	432			Part. Mech. outlet
6	18 Aug 77	70	high grate air	5.8	14.7	392	414			7.7	12.4	270	412			Part. Mech. outlet
7A	19 Aug 77	68		5.2	15.1	171	399									Gaseous only
7B				4.0	16.4	657	365									

NOTE: All parts per million (ppm) figures are corrected to a 3% O₂ constant dilution factor

#15900

GASEOUS EMISSION SUMMARY

Location: A

Fuel: _____

TEST NO.	DATE	LOAD %	CONDITIONS	MULTICLONE OUTLET						ECON. OUTLET				SO ₂ ppm Dry	SO ₃ ppm Dry	NOTES
				O ₂ % Dry	CO ₂ % Dry	CO ppm Dry	NO ppm Dry	NO ₂ ppm Wet	HC ppm Wet	O ₂ % Dry	CO ₂ % Dry	CO ppm Dry	NO ppm Dry			
7C				3.4	17.1	818	327									
7D				3.0	17.8	1050	320									
7E				5.0	15.4	137	394									
8A	20 Aug 77	65	as Found	4.8	14.9	141	417			6.4	12.9	174	403	749	5	SO _x Mech. outlet
8B		52	as Found	6.8	13.3	53	451			7.8	12.2	168	458	304	0	SO _x at Stack
			STACK EMISSIONS →							8.4	11.5	77	447			
9	23 Aug 77	61	as Found	4.9	15.6	81	367			7.8	12.0	41	383	793	3	SO _x Mech outlet
10	24 Aug 77	37	as Found	9.9	9.5	83	554			10.6	8.4	71	580			Part Mech outlet
11A	24 Aug 77	41	low grate air	7.8	12.7	41	490									Gaseous only
11B			raise grate air	8.0	12.4	56	506									
11C			raise grate air	8.5	11.6	72	541									
11D			raise grate air	9.1	11.2	99	584									
11E			raise grate air	9.5	10.6	102	597									
11F			reduce grate air	7.5	13.0	47	448									
12	24 Aug 77	45	as Found	6.1	14.5	46	414			7.3	13.0	39	380	790	5	SO _x Mech outlet
13A	25 Aug 77	77	as Found	5.2	15.1	912	502			5.8	14.2	1778	474			Gaseous only

NOTE: All parts per million (ppm) figures are corrected to a 3% O₂ constant dilution factor

#15900

GASEOUS EMISSION SUMMARY

Location: A

Fuel: _____

TEST NO.	DATE	LOAD %	CONDITIONS	Multiclone Out						Econ. Out				SO ₂ ppm Dry	SO ₃ ppm Dry	NOTES
				O ₂ % Dry	CO ₂ % Dry	CO ppm Dry	NO ppm Dry	NO ₂ ppm Wet	HC ppm Wet	O ₂ % Dry	CO ₂ % Dry	CO ppm Dry	NO ppm Dry			
13B			low grate Air	3.7	16.4	2000*	406									P.
14A	26 Aug 77	74	as found	5.4	14.5	150	455			6.5	13.3	99	448			Part. Mech Out
14B		69	" "	5.6	15.1	95	440			6.6	13.9	81	426			Brink " "
15	27 Aug 77	73	" "	4.5	15.6	264	428			5.9	13.6	393	429			Part. " "
16	30 Aug 77	59	" "	6.1	13.7	104	473			7.5	12.3	102	474			Part Mech + ESP out
17	31 Aug 77	52	" "	6.3	13.5	83	439			7.3	12.6	66	416			Part + ESP out + stack
			STACK EMISSIONS →							7.8	12.0	77	422			
18A	11 Sep 77	46	as found	7.4	11.7	62	386			8.5	10.8	58	390	886	10	Sox Mech out
18B			" "	7.1	13.0	52	409			8.6	11.5	51	422	313	5	SO _x at stack
			STACK EMISSIONS →							8.5	11.3	51	411			
19	12 Sep 77	44	as found	6.8	13.0	44	386			8.3	11.4	43	384			Brink Mech out
20	14 Sep 77	42	" "	5.3	14.8	44	306			6.9	13.1	79	294	1086	11	Sox mech outlet Brink ESP outlet

NOTE: All parts per million (ppm) figures are corrected to a 3% O₂ constant dilution factor

GASEOUS EMISSION SUMMARY

Location: A

Fuel:

TEST NO.	DATE	LOAD %	CONDITIONS	BOILER OUTLET						ECON. OUTLET				SO ₂ ppm Dry	SO ₃ ppm Dry	NOTES
				O ₂ % Dry	CO ₂ % Dry	CO ppm Dry	NO ppm Dry	NO ₂ ppm Wet	HC ppm Wet	O ₂ % Dry	CO ₂ % Dry	CO ppm Dry	NO ppm Dry			
21	23 Sep 77	82	w/o reinjection	4.5	15.8	998	392			—	—	—	—			Part boiler outlet
			MULTICLONE OUTLET EMISSIONS →							5.8	13.7	1436	391			
22	23 Sep 77	83	with reinjection	4.1	16.1	1600	362			—	—	—	—			Part boiler outlet
			MULTICLONE OUTLET EMISSIONS →							5.0	14.6	1148	367			
23	24 Sep 77	59	with reinjection	4.4	15.7	104	388			7.2	12.8	159	404			Part boiler outlet
			MULTICLONE OUTLET EMISSIONS →							5.6	14.7	158	377			
24	24 Sep 77	59	w/o reinjection	4.8	15.4	150	370			—	—	—	—			Part boiler outlet
			MULTICLONE OUTLET EMISSIONS →							5.9	14.2	157	396			

NOTE: All parts per million (ppm) figures are corrected to a 3% O₂ constant dilution factor

#15900

GASEOUS EMISSION SUMMARY

Location: AFuel: Kemmerer Coal

TEST NO.	DATE	LOAD %	CONDITIONS	Boiler Outlet						Econ. Outlet				SO ₂ ppm Dry	SO ₃ ppm Dry	NOTES
				O ₂ % Dry	CO ₂ % Dry	CO ppm Dry	NO ppm Dry	NO ₂ ppm Wet	HC ppm Wet	O ₂ % Dry	CO ₂ % Dry	CO ppm Dry	NO ppm Dry			
25	5 Oct 77	74	9" O.F. Air	5.0	14.8	450	439									Gaseous only
		1	3" O.F. Air	4.4	15.3	802	423									" "
26	6 Oct 77	70		5.05	14.8	413	446			7.3		439	381			Part. BLR OUT
		74		4.6	15.7	405	416			6.45		328	436			Part Multiclo out
27	8 Oct 77	81		4.2	15.4	1022	388			6.1		2000*	387			SASS BLR outlet
28	10 Oct 77	84	4" O.F. Air	3.9	16.4	1076	408			6.3		2000*	404			Part. BLR OUT
29	10 Oct 77	85	9" O.F. Air	3.8	15.0	480	398			6.3		429	441			" " "
30	13 Oct 77	80		4.0	—	383	460			6.6		290	506			Brink " "
31	14 Oct 77	53	5" O.F. Air	2.6	—	181	196									Gaseous
		1	Front Bottom 2"	2.6	—	293	196									
		1	Front Bottom 10"	2.6	—	117	201									
		56	5" O.F. air	3.6	—	233	243									
		1	Front Top 2"	3.5	—	231	244									
		1	Front Top 10"	3.45	—	231	239									
32	15 Oct 77	83		5.2	15.0	219	497									SASS Dir. out

NOTE: All parts per million (ppm) figures are corrected to a 3% O₂ constant dilution factor

#15900

GASEOUS EMISSION SUMMARY

Location: A

Fuel: Consolidation Coal

TEST NO.	DATE	LOAD %	CONDITIONS	BOILER OUTLET						ECON. OUTLET				SO ₂ ppm Dry	SO ₃ ppm Dry	NOTES
				O ₂ % Dry	CO ₂ % Dry	CO ppm Dry	NO ppm Dry	NO ₂ ppm Wet	HC ppm Wet	O ₂ % Dry	CO ₂ % Dry	CO ppm Dry	NO ppm Dry			
34	29 Oct 77	76	10.5" O.F. air	5.86		300	353							504	10	Blr out } SASS
										6.5		483	315	479	12	ESP out } Part.
35	30 Oct 77	76	5.5" O.F. air	5.97		313	394							410	7	Blr out } SO _x
										6.4		243	382	353	2	ESP out }
36	1 Nov 77	79	w/o reinjection	4.7	16.7	2000	344			5.6	14.8	2000+	320			Part Boiler outlet
37	1 Nov 77	87	with reinjection	5.1	15.6	276	347			5.2	15.0	319	342			Part Boiler outlet
38	2 Nov 77	59	10.5" O.F. air	4.7	15.0	61	313			7.4	12.4	66	311			Part Boiler outlet
39	2 Nov 77	60	3.0" O.F. air	4.9	14.8	670	335			6.4	13.3	1134	333			Part Boiler outlet
40	11 Nov 77	66		6.9	12.8	108	546			8.1	11.3	155	529			SASS Boiler outlet

NOTE: All parts per million (ppm) figures are corrected to a 3% O₂ constant dilution factor

#15900

GASEOUS EMISSIONS DATA

FUEL *Stansbury*

LOAD 64 %

CONDITIONS As Found

DATA TAKEN BY GLM

[illegible][illegible]

NOTE: Parts per million (ppm) figures are corrected to 3% O₂

GASEOUS EMISSIONS DATA

FUEL Stansbury
LOAD 59%
CTIONS AS found
EN BY GLM

AVERAGES										
DC out	4.2	15.7		102.8		376.7				For Test
Econ out	5.6	14.2		176		380				# 2
Stack	4.93	14.8		525		293				only

117

GASEOUS EMISSIONS DATA

FUEL STANSBURY
LOAD 61 %
TIONS LOW AIR
EN BY GLM

[illegible][illegible]

NOTE: Parts per million (ppm) figures are corrected to 3% O₂

KVB

GASEOUS EMISSIONS DATA

TEST SITE A
 TEST NO 4
 DATE 8-17-77

FUEL STANSBURY
 LOAD 60%
 CONDITIONS HIGH AIR
 DATA TAKEN BY GLM

Probe Position	Time	O ₂ % (dry)	CO ₂ % (dry)	CO		NO		HOT LINE SAMPLES, PPM (WET)								REMARKS	
				ppm(dry)		ppm(dry)		NO _x		NO		NO ₂		HC			
				unc	cor	unc	cor	unc	cor	unc	cor	unc	cor	unc	cor		
Dr Out	10:40 ^{AM}	6.3	13.6	50	61	375	460										
Stack	10:45 ^{AM}	7.9	12.0	50	69	370	509										
ESP Out		7.7	11.6	50	68	380	515										
Dr Out 1		8.2	11.2	65	92	385	543										
Dr Out 7		6.3	13.3	55	67	390	478										
Dr Out 2	11:15 ^{AM}	6.8	12.8	65	83	430	546										
Dr Out 6		5.7	14.4	55	65	355	418										
Dr Out 3		7.1	12.8	50	65	380	493										
Dr Out 5		5.3	14.5	55	63	370	425										
Dr Out 4		5.5	14.5	55	64	405	471										
Dr Out	Noon	6.1	13.9	55	67	405	490										
Stack		7.9	12.0	55	76	355	489										
Dr Out 1	1:00 ^{PM}	7.3	12.5	65	86	380	500										
Dr Out 2	1:14 ^{PM}	6.4	13.3	65	80	390	481										
Dr Out 3	1:29 ^{PM}	6.4	13.3	65	80	410	506										
Dr Out 4		6.2	13.6	70	85	445	542										
Dr Out 5		4.8	14.8	50	56	425	473										
Dr Out 4		6.4	13.9	58	72	390	481										
Dr Out 4		7.0	13.0	92	118	395	509	410	528	410	528						w Hot Line
Dr Out 4		6.0		92	111	405	486	395	475	395	475						Hot Line
Dr Out	4:30 ^{PM}	6.8															Brink Test
Dr Out	4:56 ^{PM}	7.0															Brink Test
Dr Out		7.2															Brink Test

AVERAGES

DC Out	6.3	13.6		77		497										
ESP Out	7.7	11.6		6.8		515										
Stack	7.9	12.0		72.5		499										
DC Out	6.5	13.0		114.5		497.5		501.5		501.5						Hot Line

NOTE: Parts per million (ppm) figures are corrected to 3% O₂

GASEOUS EMISSIONS DATA

FUEL STANS BURY
LOAD 72 %
TIONS LOW AIR
EN BY GLM

[illegible]

AVERAGES													
DC out		4.1	16.4		536		385						
Econ out		6.0	13.9		360		432						
Stack		6.0	13.7		1009		360						

NOTE: Parts per million (ppm) figures are corrected to 3% O₂

GASEOUS EMISSIONS DATA

FUEL STANSBURY

LOAD 70 %

CONDITIONS *HIGH AIR*

DATA TAKEN BY *Ph*

[illegible]

AVERAGES													
DC out		5.8	14.7		392		414						
Econ Out		7.7	12.4		270		412						
Stack		7.15	13.0		638		393						

NOTE: Parts per million (ppm) figures are corrected to 3% O₂

GASEOUS EMISSIONS DATA

FUEL STANBURY
LOAD 68%
CTIONS AS FOUND
EN BY GLM

[illegible]

122

KVB

GASEOUS EMISSIONS DATA

TEST SITE A
 TEST NO 8
 DATE 8-20-77

FUEL STANSBURY
 LOAD 8A - 65%
8B - 52%

CONDITIONS AS FOUND

DATA TAKEN BY GLM

Probe Position	Time	O ₂ % (dry)	CO ₂ % (dry)	CO ppm (dry)		NO ppm (dry)		HOT LINE SAMPLES, PPM (WET)								REMARKS
				unc	cor	unc	cor	NOx		NO		NO ₂		HC		
DC out	10:20 AM	4.35	15.7	500	541	340	368									8A
Stack	10:15	5.8	13.5	220	261	320	379									8A
ESP out		6.1	13.3	236	284	330	399									8A
DC out 1		5.0	14.8	50	56	360	405									8A
DC out 4		4.2	15.7	270	289	365	391									8A - SOx PROBE
DC out 7		5.1	14.5	40	45	390	442									8A
DC out 2		5.1	14.5	50	57	375	425									8A
DC out 6		4.8	14.8	122	136	375	417									8A
DC out 4		4.1	16.7	350	373	365	389									SOx PROBE
DC out 3		5.0	15.1	80	90	375	422									8A
DC out 5	11:20 AM	3.9	15.8	440	463	370	390									8A
DC out		4.8	14.9	175	196	355	394									8A
ESP out	11:40 AM	6.6	12.4	50	63	325	407									8A
Stack	11:45 AM	6.2	13.0	122	149	320	390									8A
Stack	1:30 PM	9.0	11.0	65	98	315	474									8B
DC out	2:30 PM	5.1	15.4	450	510	355	402									8B
ESP out		7.8	12.2	122	168	335	458									8B
Stack	3 PM	7.6	12.5	45	61	315	424									8B SOx PROBE
DC out 1		7.5	12.4	40	53	370	494									8B
DC out 2		6.9	13.0	40	51	355	454									8B
DC out 3		6.8	13.3	40	51	355	451									8B
DC out 4		6.4	13.9	50	62	350	432									8B
Stack	3:25 PM	8.6	11.0	50	73	305	444									8B SOx PROBE
DC out 5		6.4	13.9	40	49	345	426									8B
DC out		4.8	14.9		141		417									Average for 8A
Econ out		6.4	12.9		174		403									8A
Stack		6.0	13.25		205		384.5									8A
SOx Probe		4.15	15.7		331		390									8A

AVERAGES

DC out	6.8	13.3		53		451										Average for 8B
Econ out	7.8	12.2		168		458										8B
Stack	8.4	11.5		77.3		447.3										8B
SOx Probe	8.1	11.35		67.0		434										Stack SOx 8B

NOTE: Parts per million (ppm) figures are corrected to 3% O₂

GASEOUS EMISSIONS DATA

FUEL STANBURY
LOAD 61 %
CTIONS AS FOUND
EN BY GLM

[illegible]

AVERAGES													
DC out	4.9	15.6		81		367							
Econ out	7.8	12.0		41		383							
Stack	7.6	12.2		98.3		433							
SO ₂ Probe	5.15	14.95		113.5		366.5							

NOTE: Parts per million (ppm) figures are corrected to 3% O₂

GASEOUS EMISSIONS DATA

FUEL 5 Tanks burn v

LOAD 37

CONDITIONS *as found*

DATA TAKEN BY GLM

[illegible][illegible]

NOTE: Parts per million (ppm) figures are corrected to 3% O₂

GASEOUS EMISSIONS DATA

FUEL 5 Fansbury

LOAD 41

CONDITIONS Varv Excess Air

DATA TAKEN BY GLM

AVERAGES

[illegible]

126

15900

GASEOUS EMISSIONS DATA

DATA TAKEN BY G L M.

KVB

GASEOUS EMISSIONS DATA

TEST SITE ABMA Site A

FUEL Stansbury

TEST NO 14 A & B

LOAD 14-A - 24 / 14-B - 69

DATE 8-26-77

CONDITIONS 14-A High OFA 14-B as Found

DATA TAKEN BY GLM

Probe Position	Time	O ₂ % (dry)	CO ₂ % (dry)	CO - ppm (dry)		NO ppm (dry)		HOT LINE SAMPLES, PPM (WET)								REMARKS
								NOx		NO		NO ₂		HC		
				unc	cor	unc	cor	unc	cor	unc	cor	unc	cor	unc	cor	
14FA																
Comp		5.0	15.1	110	124	390	434									
inlet	9:35 AM	6.5	13.3	80	99	360	448									
Stack		6.5	13.3	122	152	350	438									
#1		6.7	13.0	92	116	370	479									
#2		5.4	14.5	180	173	375	445									
#3	10:05 AM	4.6	15.4	330	362	385	422									
#4		4.7	15.4	160	177	395	486									
#5		5.4	14.5	60	69	405	468									
#7		6.0	13.6	70	84	410	493									
Stack	10:15 AM	6.5	13.0	140	236	355	441									
Comp	11:20 AM	5.0	15.4	420	473	370	417									
Comp		7.0	15.4	350	394	350	394									
#12367		5.7	14.5	122	144	290	392									
Comp	3:30 PM	6.4	13.6	92	118	350	448									
#3		6.4	14.2	92	114	380	469									
Stack		6.6	13.9	125	156	370	410									
inlet		6.6	13.9	65	81	340	426									
#1	4:10 PM	5.8	14.5	95	113	370	439									
#2		6.1	14.8	85	103	380	462									
#4		5.5	15.4	80	93	390	453									
#12367		5.4	15.7	125	144	350	410									
#6		5.0	16.0	70	79	375	422									
#7		4.9	16.0	60	67	355	398									
Stack		6.5	13.4		181		426									

AVERAGES

14A inlet	-	5.4	14.5	150	155	455										Part mech out
Econ out	-	6.5	13.3	99	118	448										"
14B inlet	-	5.6	15.1	95	114	410										Brink mech out
Econ out	-	6.6	13.9	81	103	426										"

NOTE: Parts per million (ppm) figures are **129** corrected to 3% O₂

GASEOUS EMISSIONS DATA

FUEL Stansbury

LOAD 73

CONDITIONS *low Air*

DATA TAKEN BY _____

[illegible]

AVERAGES													
Mgt Fin	4.5	15.6		264		428							
Econ out	5.9	13.6		393		429							
Stack	5.85	13.8		309		428							

NOTE: Parts per million (ppm) figures are corrected to 3% O₂

GASEOUS EMISSIONS DATA

FUEL Stansbury & Kemmer

LOAD 59

CONDITIONS *As Found*

DATA TAKEN BY GLM

[illegible][illegible]

NOTE: Parts per million (ppm) figures are corrected to 3% O₂

GASEOUS EMISSIONS DATA

DATA TAKEN BY GLM

[illegible][illegible]

NOTE: Parts per million (ppm) figures are corrected to 3% O₂

GASEOUS EMISSIONS DATA

DATA TAKEN BY G L M

[illegible]

19A		AVERAGES											
Multi- Clone out		7.4	11.7		62		386						
Econ-out		8.5	10.8		58		340						
Multi- Clone out		7.1	19.0		52		409						
Econ out		8.6	11.5		51		422						

NOTE: Parts per million (ppm) figures are corrected to 3% O₂

GASEOUS EMISSIONS DATA

FUEL Stansbury

LOAD 44

CONDITIONS as Found

DATA TAKEN BY GLM

NOTE: Parts per million (ppm) figures are corrected to 3% O₂

GASEOUS EMISSIONS DATA

FUEL Kemmerer Coal

LOAD 80%

CONDITIONS Without Fly Ash re-injection

DATA TAKEN BY JEC

[illegible][illegible]

NOTE: Parts per million (ppm) figures are corrected to 3% O₂

GASEOUS EMISSIONS DATA

TEST SITE ABMA-SITE A

FUEL Kimmerer Coal

TEST NO 24

LOAD 60%

DATE 9/24/77

CONDITIONS A₃ found - W/O flash reinsertion

DATA TAKEN BY JEC

[illegible]

AVERAGES													
BLR OUT		4.8	15.4		150		370		2.59		293		
DC OUT		5.9	14.2		157		396						
Stack		7.5	12.2		163		400						

NOTE: Parts per million (ppm) figures are corrected to 3% O₂

GASEOUS EMISSIONS DATA

FUEL Kennecott Coal

LOAD 70% A 74% B

CONDITIONS As Found

DATA TAKEN BY J.B.

AVERAGES

BLR OUT		5.05	14.8		413		446					Totat 26A
ECON OS		7.3	12.1		439		381					" "
BLR OUT		4.6	15.7		405		416					Total 26B
ECON OUT		6.95	12.9		328		436					" "

NOTE: Parts per million (ppm) figures are corrected to 3% O₂

GASEOUS EMISSIONS DATA

TEST SITE ABMA - SITE A

FUEL Kennecott Coal

TEST NO 27

LOAD 81%

DATE 10/8/77

CONDITIONS As found

DATA TAKEN BY J E C

[illegible]

AVERAGES

[illegible]

NOTE: Parts per million (ppm) figures are corrected to 3% O₂

GASEOUS EMISSIONS DATA

DATA TAKEN BY RAP

[illegible]

		AVERAGES															
BUROUT		4.0	15.0		383		460										
ECON OUT		6.6	12.3		429		441										
Stack		6.5	13.3		410		576										
DCont		5.3	14.6		299.8		501										

NOTE: Parts per million (ppm) figures are corrected to 3% O₂

GASEOUS EMISSIONS DATA

DATA TAKEN BY PLL

AVERAGES

[illegible]

146

GASEOUS EMISSIONS DATA

FUEL Kemmerer Coal

LOAD 83%

CONDITIONS as found

DATA TAKEN BY JOB

[illegible]

AVERAGES

BLR OUT	5.2	15.0		219		497							
PC OUT	5.4	14.8		545		483							
ECON OUT	6.4	13.2		290		486							

NOTE: Parts per million (ppm) figures are corrected to 3% O₂

GASEOUS EMISSIONS DATA

FUEL Consolidation Coal
LOAD 87%
TIONS With reinjection
EN BY J.O.B.

[illegible]

AVERAGES													
BLR 005		5.00	15.6		276		347						
Eco 005		5.2	14.95		319		242						
Stack		5.5	15.1		406		337						

NOTE: Parts per million (ppm) figures are corrected to 3% O₂

GASEOUS EMISSIONS DATA

FUEL Consolidation Coal

LOAD 60%

CONDITIONS 3" O.F.A.

DATA TAKEN BY DEC

[illegible][illegible]

NOTE: Parts per million (ppm) figures are corrected to 3% O₂

KVB

GASEOUS EMISSIONS DATA

TEST SITE A FUEL Kemmerer
 TEST NO 40 LOAD 66%
 DATE 11/11/77 CONDITIONS as found
 DATA TAKEN BY J.E.C.

Probe Position	Time	O ₂ (dry)	CO ₂ (dry)	CO ppm(dry)		NO ppm(dry)		HOT LINE SAMPLES, PPM (WET)								REMARKS	
				unc		unc		NOx		NO		NO ₂		HC			
				unc	cor	unc	cor	unc	cor	unc	cor	unc	cor	unc	cor		
Comp 4-7	10:12	7.0	12.8	80	103	395	508										
# 4	11:05	6.3	13.6	80	59	410	539										
# 5	11:15	7.0	12.8	80	103	415	546										
# 6	11:30	6.5	13.3	40	50	415	528										
# 7	11:45	6.5	12.8	92	114	410	447										
scrubber inlet	12:00	7.8	11.6	92	125	370	505										
4-7	12:15	6.3	13.3	80	98	4120	514										
Comp 1-3	12:45	7.2	12.8	110	143	460	600										
# 4	1:25	6.1	13.6	80	97	4140	532										
# 5	1:40	6.3	12.2	90	110	4100	490										
# 6	2:55	6.8	12.8	40	51	470	596										
# 7	3:10	7.0	12.4	122	157	390	501										
scrubber inlet	3:35	8.0	11.3	140	134	390	510										
4-7	4:35	7.4	12.3	90	119	420	556										
scrubber inlet	4:47	8.6	11.0	160	145	375	544										
# 4	4:41	7.3	12.2	105	132	415	545										
# 5	5:00	7.6	12.1	105	141	415	625										
# 6	5:10	7.8	13.6	40	47	470	557										
# 7	5:30	7.6	12.0	105	141	410	601										
4-7	5:42	8.1	11.6	105	147	430	600										

AVERAGES

Boiler out	6.4	12.8	104	104	395	546										
Econ out	8.1	11.3	155	155	375	529										

NOTE: Parts per million (ppm) figures are corrected to 3% O₂

SOx DATA SUMMARY

Test No.	Load	O2 (%)	SO2 (unc ppm)	SO3 (unc ppm)	SOx (unc ppm)	SO2 (corr ppm)	SO3 (corr ppm)	SOx (corr ppm)	Test Description
1A	191,000	3.6	735	0	735	765	-0-	765	BASELINE
1B	"	3.6	760	7	767	791	8	799	BLR OUTLET,
1C	"	3.6	720	-0-	720	749	0	749	AS FOUND ON
1AVE.	"	3.6	738	2	740	762	2	(771)	
8A	196,000	4.2	705	3.8	709	756	4	760	
8B	"	4.2	703	9.3	712	754	10	764	
8C	"	4.1	691	-0-	691	736	-0-	736	
AVE	"	4.2	700	4.4	704	749	4.7	(753)	
8D	156,000	7.6	230	0.35	230	309	0.5	310	
8E	155 " 155	8.6	208	-0-	208	302	-0-	302	
8F	"	8.6	208	-0-	208	302	-0-	302	
AVE	"	8.3	215	0.1	215	304	0.2	(305)	
9A	182,000	4.5	712	2.1	714	777	2.3	779	
9B	"	5.8	561	3.2	564	665	3.8	669	
9C	"	5.8	791	3.2	794	938	3.8	942	
AVE	"	5.4	688	2.8	691	793	3.3	(797)	
12A	141,000	5.76	650	1.6	652	769	1.9	771	
12B	"	5.4	648	4.5	653	748	5.2	753	
12C	"	5.36	735	5.6	741	852	6.4	858	
AVE	"	5.5	678	3.9	682	790	4.5	(794)	

SOx DATA SUMMARY

[illegible]

SOx DATA SUMMARY

Test No.	Load	O2 (%)	SO2 (unc ppm)	SO3 (unc ppm)	SOx (unc ppm)	SO2 (corr ppm)	SO3 (corr ppm)	SOx (corr ppm)	Test Description
34A	76%	6.0	429	9	438	515	11	526	BLR-OUT
34B	"	6.4	430	6	436	530	8	538	↓
34C	"	6.2	385	8	393	468	10	478	
AVE	"	6.2	415	8	422	504	10	514	
34D	"	6.4	594	10	604	732	12	744	ESP OUT
34E	"	6.6	382	8	396	484	10	494	↓
34F	"	6.8	373	11	384	473	14	487	
AVE	"	6.6	452	10	461	563	12	575	
35A	76%	6.0	336	7	343	404	8	412	BLR OUT
35B	"	5.85	344	5	349	408	6	414	↓ ↓
35C	"	6.0	348	6	354	417	7	424	
AVE	"	5.95	343	6	349	410	7	417	
35D	"	6.4	285	0	285	352	0	352	ESP OUT
35E	"	6.5	284	3	287	353	4	357	↓ ↓
35F	"	6.4	288	2	290	355	3	358	
AVE	"	6.47	286	2	287	353	2	356	

Local ARMA - SITE ASOx DATA SHEETDate 8-9-77 Probe Location & Probe Length 2.5' mech. OUTUnit # 2 Fuel STANSBURY COAL Load 59%

Test Description: _____

Test No.	Box No.	Sample Time	Meter Temp. (T)	Meter (P) Press.	Meter Reading	(P) Baro. Press.	Port	Purge Time	O2
1A	3	11:07	104	-0-	0.000	2357	4	11:28	
		11:21	106	-0-	1.000			12:02	3.6
1B	2	11:35	107	-0-	0.000		}	12:04	
		11:49	108	-0-	1.000			12:34	
1C	1	11:59	110	-0-	0.000		}	13:05	
		12:15	111	-0-	1.000			13:40	

SAMPLED BY _____

Test # 1ATest # 1BTest # 1C

	SO2	SO3	SOx	SO2	SO3	SOx	SO2	SO3	SOx
Normality N	.0094	.0092	.0094	.0093					
Dilution Factor F	10	1		10	1		10	1	
SPIKE Blank B	4.9								
	5.9								
	4.5								
Averages	5.1								
Ml. of Titrant A	18.7	3.5		18.5	6.3		17.7	5.0	
	18.5			19.1			18.6		
	18.8			19.6			18.7		
Averages	18.7	3.5		19.1	6.3		18.3	5.0	
460 + T	565			567			570		
Sample Vol. V	1ft ³			1ft ³			1ft ³		
P + p									
A - B	13.6	-1.6		14.0	1.2		13.2	-1	

TITRATED BY _____

$$SO_2 = \frac{(A-B)(N)(F)(460+T)(24)}{V(P+p)}$$

$$SO_2 = \frac{(13.6)(.0094)(10)(565)(24)}{(1)(22.57)}$$

$$SO_2 = \boxed{735.4} \quad SO_3 = \boxed{0}$$

$$SO_3 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_2 @ 3\% O_2 = \underline{765}$$

$$SO_3 @ 3\% O_2 = \underline{0}$$

$$SO_x @ 3\% O_2 = \underline{765}$$

$$SO_2 = \frac{(14.0)(.0094)(10)(567)(24)}{(1)(22.57)}$$

$$SO_2 = \boxed{759.8}$$

$$SO_3 = \frac{(1.2)(.0094)(1)(567)(24)}{(1)(22.57)}$$

$$SO_3 = \boxed{6.5}$$

$$SO_2 @ 3\% O_2 = \underline{790.5}$$

$$SO_3 @ 3\% O_2 = \underline{6.7}$$

$$SO_x @ 3\% O_2 = \underline{797.2}$$

$$SO_2 = \frac{(13.2)(.0094)(10)(570)(24)}{(1)(22.57)}$$

$$SO_2 = \boxed{720.2}$$

$$SO_3 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_3 = \boxed{0}$$

$$SO_2 @ 3\% O_2 = \underline{749.3}$$

$$SO_3 @ 3\% O_2 = \underline{0}$$

$$SO_x @ 3\% O_2 = \underline{749.3}$$

Local ABMA - SITE ASOx DATA SHEETDate 8/20/77 Probe Location & Probe Length 2.5(+ Multicline OUTUnit # 1 Fuel STANESBURY COAL Load 65%

Test Description:

Test No.	Box No.	Sample Time	Meter Temp. (T)	Meter (P) Press.	Meter Reading	(P) Baro. Press.	Port	Purge Time	O2
8A	1	9:59	9	0	0.000	24.02	4	10:17	
		10:12	100		1.000			10:41	4.2
8B	3	10:31	101		0.000			10:48	"
		10:44	102		1.000			11:18	"
8C	2	11:04	103		0.000			11:22	4.1
		11:17	104		1.000			11:52	

SAMPLED BY

Test # 8ATest # 8BTest # 8C

	SO2	SO3	SOx	SO2	SO3	SOx	SO2	SO3	SOx
Normality N	.00979								
Dilution Factor F	10	1		10	1		10	1	
SPIKE B	4.8 4.8 4.9								
Averages	4.833								
Ml. of Titrant A	17.8 17.7 17.7	4.9		17.8 17.6 17.5	5.0		17.4 17.3 17.4	4.8	
Averages	17.733			17.633			17.367		
460 + T	559			561.5			563.5		
Sample Vol. V	1.0 (1)			1.0			1.0		
P + p	24.02			24.02			24.02		
A - B	12.90	107		12.80	17		12.53	0	

TITRATED BY

$$SO_2 = \frac{(A-B)(N)(F)(460+T)(24)}{V(P+p)}$$

$$SO_2 = \frac{(12.9)(.00979)(10)(559)(24)}{(1)(24.02)}$$

$$SO_2 = \boxed{705} \quad SO_3 = \boxed{3.9}$$

$$SO_3 = \frac{(107)(.00979)(1)(561.5)(24)}{(1)(24.02)}$$

$$SO_2 @ 3\% O_2 = \underline{756}$$

$$SO_3 @ 3\% O_2 = \underline{4}$$

$$SO_x @ 3\% O_2 = \underline{760 ppm}$$

$$SO_2 = \frac{(12.8)(.00979)(10)(561.5)(24)}{(1)(24.02)}$$

$$SO_2 = \boxed{703}$$

$$SO_3 = \frac{(17)(.00979)(1)(561.5)(24)}{(1)(24.02)}$$

$$SO_3 = \boxed{9.3}$$

$$SO_2 @ 3\% O_2 = \underline{754}$$

$$SO_3 @ 3\% O_2 = \underline{10}$$

$$SO_x @ 3\% O_2 = \underline{764}$$

$$SO_2 = \frac{(12.53)(.00979)(10)(563.5)(24)}{(1)(24.02)}$$

$$SO_2 = \boxed{691}$$

$$SO_3 = \frac{(0)(.00979)(1)(563.5)(24)}{(1)(24.02)}$$

$$SO_3 = \boxed{0}$$

$$SO_2 @ 3\% O_2 = \underline{736}$$

$$SO_3 @ 3\% O_2 = \underline{0}$$

$$SO_x @ 3\% O_2 = \underline{736}$$

Local ABMA-SITE A

SOx DATA SHEET

Date 8/20/77 Probe Location & Probe Length 2.5 ft. StackUnit # 1 Fuel Stansbury Coal Load 52%

Test Description:

Test No.	Box No.	Sample Time	Meter Temp. (T)	(P) Press.	Meter Reading	(P) Baro. Press.	Port	Purge Time	O2
8D	1	14:23	84	-0-	0.000	23.92	SE stack		
		14:39	84		1.000				7.6
8E	3	14:52	86		0.000				
		15:06	86		1.000				1.6
8F	2	15:21	85		0.000				
		15:34	86		1.000				

SAMPLED BY

Test # 8PTest # 8ETest # 8F

	SO2	SO3	SOx	SO2	SO3	SOx	SO2	SO3	SOx
Normality N	0.00979								
Dilution Factor F	10			10			10		
Blank B	0	SPECK		0			0		
Averages		4.833			4.833			4.833	
Ml. of Titrant A	4.3			3.8			3.8		
	4.3	4.9		3.9	4.8		3.9	4.9	
	—			3.9			3.9		
Averages	4.3			3.87			3.87		
460 + T	544			546			544		
Sample Vol. V									
P + p	23.92			23.92			23.92		
A - B	4.3	0		3.87	0		3.87	0	

TITRATED BY

$$SO_2 = \frac{(A-B)(N)(F)(460+T)(24)}{V(P+p)}$$

$$SO_2 = \frac{(4.3)(0.00979)(10)(544)(24)}{(1)(1)(1)(23.92)}$$

$$SO_2 = \boxed{230} \quad SO_3 = \boxed{.25}$$

$$SO_3 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)(\quad)}$$

$$SO_2 @ 3\% O_2 = \underline{309}$$

$$SO_3 @ 3\% O_2 = \underline{.5}$$

$$SO_x @ 3\% O_2 = \underline{310}$$

$$SO_2 = \frac{(3.87)(\quad)(\quad)(\quad)(546)(24)}{(\quad)(\quad)(\quad)}$$

$$SO_2 = \boxed{208}$$

$$SO_3 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)(\quad)}$$

$$SO_3 = \boxed{0}$$

$$SO_2 @ 3\% O_2 = \underline{302}$$

$$SO_3 @ 3\% O_2 = \underline{0}$$

$$SO_x @ 3\% O_2 = \underline{302}$$

160

$$SO_2 = \frac{(\quad)(\quad)(\quad)(\quad)(544)(24)}{(\quad)(\quad)(\quad)}$$

$$SO_2 = \boxed{208}$$

$$SO_3 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)(\quad)}$$

$$SO_3 = \boxed{0}$$

$$SO_2 @ 3\% O_2 = \underline{302}$$

$$SO_3 @ 3\% O_2 = \underline{0}$$

$$SO_x @ 3\% O_2 = \underline{302}$$

Load unsteady

SOx DATA SHEET

Local ABMA - SITE ADate 8/22/77 Probe Location & Probe Length 2.5' BIR OUTUnit # 1 Fuel STANBURY COAL Load 61%Test Description: only SO₂ samples were spiked

Test No.	Box No.	Sample Time	Meter Temp. (T)	Meter (P) Press.	Meter Reading	(P) Baro. Press.	Port	Purge Time	O ₂
9A	1	14:10	101	-0-	0.000	23.44	4	14:25	
		14:23	102		1.000			14:35	4.5
9B	3	14:35	105		0.000			14:55	
		14:48	105		1.000			14:25	5.8
9C	2	15:02	104		0.000			14:25	
		15:16	104		1.000				

SAMPLED BY

Test # 9ATest # 9BTest # 9C

	SO ₂	SO ₃	SO _x	SO ₂	SO ₃	SO _x	SO ₂	SO ₃	SO _x
Normality N									
Dilution Factor F	10	1		10	1		10	1	
Spikes Blank B		4.1 4.2 4.3							
Averages		4.23							
Ml. of Titrant A	12.7 12.6	4.6		10.0 9.9 9.8	4.8		14.0 14.0 14.0	4.0	
Averages	12.65	4.6		9.9	4.8		14.0	4.8	
460 + T	561.5								
Sample Vol. V	1.000								
P + p	23.44								
A - B	12.65	0.37		9.9	0.57		14.0	0.57	

TITRATED BY

$$SO_2 = \frac{(A-B)(N)(F)(460+T)(24)}{V(P+p)}$$

$$SO_2 = \frac{(12.65)(0.0099)(10)(561.5)(24)}{(1.0)(23.44)}$$

$$SO_2 = \boxed{712} \quad SO_3 = \boxed{2.1}$$

$$SO_3 = \frac{(0.37)(1.0)(10)(561.5)(24)}{(1.0)(23.44)}$$

$$SO_2 @ 3\% O_2 = \underline{777}$$

$$SO_3 @ 3\% O_2 = \underline{2.3}$$

$$SO_x @ 3\% O_2 = \underline{779}$$

$$SO_2 = \frac{(9.9)(0.0099)(10)(565)(24)}{(1.0)(23.44)}$$

$$SO_2 = \boxed{561}$$

$$SO_3 = \frac{(0.57)(1.0)(10)(565)(24)}{(1.0)(23.44)}$$

$$SO_3 = \boxed{3.2}$$

$$SO_2 @ 3\% O_2 = \underline{664.6}$$

$$SO_3 @ 3\% O_2 = \underline{3.8}$$

$$SO_x @ 3\% O_2 = \underline{669}$$

$$SO_2 = \frac{(14.0)(0.0099)(10)(564)(24)}{(1.0)(23.44)}$$

$$SO_2 = \boxed{791}$$

$$SO_3 = \frac{(0.57)(1.0)(10)(564)(24)}{(1.0)(23.44)}$$

$$SO_3 = \boxed{3.2}$$

$$SO_2 @ 3\% O_2 = \underline{938}$$

$$SO_3 @ 3\% O_2 = \underline{3.9}$$

$$SO_x @ 3\% O_2 = \underline{942}$$

Local ABMA SITE ASOx DATA SHEETDate 8/24/77 Probe Location & Probe Length 2.5 ft. MECH. OUTUnit # 1 Fuel STANBURY COAL Load 41%Test Description: #12

Test No.	Box No.	Sample Time	Meter Temp. (T)	Meter (P) Press.	Meter Reading	(P) Baro. Press.	Port	Purge Time	O2
12A	2	15:52	96	-0-	0.000	23.81	4	15:10	5.1 / 5.9
		15:05	96		1.000			15:40	5.7
12B	1	15:17	97		0.000			15:45	5.5 / 5.6
			97		1.000			16:15	5.1
12C	3	15:42	93		0.000			16:15	5.4 / 5.6
		15:55	92		1.000			16:45	5.1

SAMPLED BY

Test #12A

Test #12B

Test #12C

	SO2	SO3	SOx	SO2	SO3	SOx	SO2	SO3	SOx
Normality N	.0100								
Dilution Factor F	10	1		10	1		10	1	
Blank B		6.3							
		6.4							
		6.3							
Averages		6.3							
Ml. of Titrant A	11.7	6.6		11.4	2.1		13.2	2.3	
	11.6			11.6			13.1		
	11.6			11.6			13.2		
Averages	11.6	6.6		11.53			13.2		
460 + T	556			557					
Sample Vol. V	1.000								
P + p	23.81								
A - B	X	.3		X	0.8		X	1.0	

TITRATED BY

$$SO_2 = \frac{(A-B)(N)(F)(460+T)(24)}{V(P+p)}$$

$$SO_2 = \frac{(11.6)(.01)(10)(556)(24)}{(1.000)(1)}$$

$$SO_2 = \boxed{650} \quad SO_3 = \boxed{1.6}$$

$$SO_3 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_2 @ 3\% O_2 = \underline{767.5}$$

$$SO_3 @ 3\% O_2 = \underline{1.89}$$

$$SO_x @ 3\% O_2 = \underline{771}$$

$$SO_2 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_2 = \boxed{647.5}$$

$$SO_3 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_3 = \boxed{4.5}$$

$$SO_2 @ 3\% O_2 = \underline{749}$$

$$SO_3 @ 3\% O_2 = \underline{5.2}$$

$$SO_x @ 3\% O_2 = \underline{753}$$

162

$$SO_2 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_2 = \boxed{735.1}$$

$$SO_3 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_3 = \boxed{5.56}$$

$$SO_2 @ 3\% O_2 = \underline{852}$$

$$SO_3 @ 3\% O_2 = \underline{6.4}$$

$$SO_x @ 3\% O_2 = \underline{858}$$

Local ARMA-SITEA

SOx DATA SHEET

Date 9/11/77 Probe Location & Probe Length 2.5' ESP InletUnit # 1 Fuel Stansbury Coal Load 48%

Test Description: _____

Test No.	Box No.	Sample Time	Meter Temp. (T)	Meter (P) Press.	Meter Reading	(P) Baro. Press.	Port	Purge Time	O2
18A	3	11:23	107	-0-	0.000	23.78	4	11:42	
			107	}	1.000			12:12	6.8
11B	1	11:58	107	}	0.000	}	}	12:15	
			106	}	1.000			12:45	7.0
18C	2	12:27	106	}	0.000	}	}	12:45	
			106	↓	1.000			13:15	6.9

SAMPLED BY _____

Test # 18ATest # 18BTest # 18C

	SO2	SO3	SOx	SO2	SO3	SOx	SO2	SO3	SOx
Normality N	0.004								
Dilution Factor F	10	1		10	1		10	1	
SPIKE Blank B		6.6							
		6.7							
Averages		6.6							
Ml. of Titrant A	11.5	7.9		11.7	8.2		12.0	7.6	
	11.2			11.8			11.8		
	11.4			11.7			11.9		
Averages	11.4	7.9		11.7	8.2		11.9	7.6	
460 + T	566			566			566		
Sample Vol. V	14 ³			14 ³			14 ³		
P + p	23.78			23.78			23.78		
A - B	—	1.3		—	1.6		—	1.0	

TITRATED BY _____

$$SO_2 = \frac{(A-B)(N)(F)(460+T)(24)}{V(P+p)}$$

$$SO_2 = \frac{(11.4)(0.004)(10)(566)(24)}{(1)(23.78)}$$

$$SO_2 = \boxed{677.3} \quad SO_3 = \boxed{7.72}$$

$$SO_3 = \frac{(1.3)(0.004)(1)(566)(24)}{(1)(23.78)}$$

$$SO_2 @ 3\% O_2 = \underline{860}$$

$$SO_3 @ 3\% O_2 = \underline{9.8}$$

$$SO_x @ 3\% O_2 = \underline{870}$$

$$SO_2 = \frac{(11.7)(0.004)(10)(566)(24)}{(1)(23.78)}$$

$$SO_2 = \boxed{695.1}$$

$$SO_3 = \frac{(1.6)(0.004)(1)(566)(24)}{(1)(23.78)}$$

$$SO_3 = \boxed{9.51}$$

$$SO_2 @ 3\% O_2 = \underline{894}$$

$$SO_3 @ 3\% O_2 = \underline{12.2}$$

$$SO_x @ 3\% O_2 = \underline{906}$$

163

$$SO_2 = \frac{(11.9)(0.004)(10)(566)(24)}{(1)(23.78)}$$

$$SO_2 = \boxed{706.96}$$

$$SO_3 = \frac{(1.0)(0.004)(1)(566)(24)}{(1)(23.78)}$$

$$SO_3 = \boxed{5.94}$$

$$SO_2 @ 3\% O_2 = \underline{903}$$

$$SO_3 @ 3\% O_2 = \underline{7.6}$$

$$SO_x @ 3\% O_2 = \underline{911}$$

Local ADMA-SITE ASOx DATA SHEETDate 9/11/77 Probe Location & Probe Length 2.5' StackUnit # 1 Fuel Stansbury Coal Load 48%

Test Description:

Test No.	Box No.	Sample Time	Meter Temp. (T)	Meter (P) Press.	Meter Reading	(P) Baro. Press.	Port	Purge Time	O2
18D	2	16:10	63	-0-	0.000	23.75	SE Stack		8.7
		16:23	62		1.000				
18E	3	16:42	61		0.000				
		16:57	61		1.000				8.2
18F	1	17:09	61		0.000				
		17:22	61		1.000				

SAMPLED BY

Test # 18DTest # 18ETest # 18F

	SO2	SO3	SOx	SO2	SO3	SOx	SO2	SO3	SOx
Normality N	0.0104								
Dilution Factor F	10	1		10	1		10	1	
Spike Blank B		6.5 6.6 6.6							
Averages		6.6							
Ml. of Titrant A	4.0 4.1 4.3	7.0		3.7 3.8 —	7.2		4.3 4.1 4.2	7.4	
Averages	4.1			3.7			4.2		
460 + T	523			521			521		
Sample Vol. V	16 ⁺								
P + p	23.75								
A - B	—	0.4		—	0.6		—	0.9	

TITRATED BY

$$SO_2 = \frac{(A-B)(N)(F)(460+T)(24)}{V(P+p)}$$

$$SO_2 = \frac{(4.1)(0.0104)(10)(523)(24)}{(1)(23.75)}$$

$$SO_2 = \boxed{225.4} \quad SO_3 = \boxed{2.2}$$

$$SO_3 = \frac{(0.4)(0.0104)(1)(523)(24)}{(1)(23.75)}$$

$$SO_2 @ 3\% O_2 = \underline{330}$$

$$SO_3 @ 3\% O_2 = \underline{4}$$

$$SO_x @ 3\% O_2 = \underline{334}$$

$$SO_2 = \frac{(3.7)(0.0104)(10)(521)(24)}{(1)(23.75)}$$

$$SO_2 = \boxed{202.6}$$

$$SO_3 = \frac{(0.6)(0.0104)(1)(521)(24)}{(1)(23.75)}$$

$$SO_3 = \boxed{3.28}$$

$$SO_2 @ 3\% O_2 = \underline{285}$$

$$SO_3 @ 3\% O_2 = \underline{5}$$

$$SO_x @ 3\% O_2 = \underline{290}$$

164

$$SO_2 = \frac{(4.2)(0.0104)(10)(521)(24)}{(1)(23.75)}$$

$$SO_2 = \boxed{230.0}$$

$$SO_3 = \frac{(0.9)(0.0104)(1)(521)(24)}{(1)(23.75)}$$

$$SO_3 = \boxed{4.38}$$

$$SO_2 @ 3\% O_2 = \underline{323}$$

$$SO_3 @ 3\% O_2 = \underline{6}$$

$$SO_x @ 3\% O_2 = \underline{329}$$

Local ABMA SITE ASOx DATA SHEETDate 9/14/77 Probe Location & Probe Length 2.54 outUnit # 1 Fuel Kennecott coal Load 245% Low O₂Test Description: meter corr. factor = 1.03

Test No.	Box No.	Sample Time	Meter Temp. (T)	Meter (P) Press.	Meter Reading	(P) Baro. Press.	Port	Purge Time	O ₂
20A		START	105	-0-	0.000	23.86	#4		5.6%
		FINISH	105		1.000				5.4%
20B		S	110		0.000				6.0%
		F	111		1.000				6.0%
20C		S	111		0.000				6.3%
		F	111		1.000				6.8

SAMPLED BY

Test # 20ATest # 20BTest # 20C

	SO ₂	SO ₃	SO _x	SO ₂	SO ₃	SO _x	SO ₂	SO ₃	SO _x
Normality N	.0141								
Dilution Factor F	10	1		10	1		10	1	
Spike Blank B		6.2							
Averages		6.2							
Ml. of Titrant A	13.8 14.0 14.1	6.8		11.1 11.6 11.0	7.5		9.5 9.6 9.6	7.8	
Averages	13.96	6.8		11.23	7.5		9.57		
460 + T	565			570.5			571		
Sample Vol. V	1.03								
P + p	23.86								
A - B	—	0.4		—	1.3		—	1.6	

TITRATED BY

$$SO_2 = \frac{(A-B)(N)(F)(460+T)(24)}{V(P+p)}$$

$$SO_2 = \frac{(13.96)(.0141)(10)(565)}{(1.03)(23.86)} 24$$

$$SO_2 = \boxed{1086} \quad SO_3 = \boxed{3.0}$$

$$SO_3 = \frac{() () () () () 24}{() () ()}$$

$$SO_2 @ 3\% O_2 = \underline{1262}$$

$$SO_3 @ 3\% O_2 = \underline{3.5}$$

$$SO_x @ 3\% O_2 = \underline{1265}$$

$$SO_2 = \frac{(11.23)(.0141)(10)(570.5)}{(1.03)(23.86)} 24$$

$$SO_2 = \boxed{882}$$

$$SO_3 = \frac{() () () () () 24}{() () ()}$$

$$SO_3 = \boxed{10}$$

$$SO_2 @ 3\% O_2 = \underline{1059}$$

$$SO_3 @ 3\% O_2 = \underline{12}$$

$$SO_x @ 3\% O_2 = \underline{1071}$$

$$SO_2 = \frac{(9.57)(.0141)(10)(571)}{(1.03)(23.86)} 24$$

$$SO_2 = \boxed{752}$$

$$SO_3 = \frac{() () () () () 24}{() () ()}$$

$$SO_3 = \boxed{12.6}$$

$$SO_2 @ 3\% O_2 = \underline{938}$$

$$SO_3 @ 3\% O_2 = \underline{16}$$

$$SO_x @ 3\% O_2 = \underline{954}$$

SOx DATA SHEETDate 10/29/11 Probe Location & Probe Length 18" BLR OUTUnit # 1 Fuel Consolidation Coal Load 80%Test Description: SAs, SOx Port in + out ESP Opt. conditions

Test No.	Box No.	Sample Time	Meter Temp. (T)	Meter (P) Press.	Meter Reading*	(P) Baro. Press.	Port	Purge Time	O2
34A	1	13:04	87	-0-	0.000	23.62	4	13:30	6.0
		13:17	112		1.000			14:00	
34B	2	13:45	98		0.000			16:02	6.4
		13:56	116		1.000			16:31	
34C	3	14:32	100		0.000			14:52	
		14:46	113		1.000			15:22	6.2

SAMPLED BY _____

* Meter Corr. 1.036

Test # 34ATest # 34BTest # 34C

	SO2	SO3	SOx	SO2	SO3	SOx	SO2	SO3	SOx
Normality N	.0141								
Dilution Factor F	10	1		10	1		10	1	
Blank B	.05	Spike 6.6							
Averages	.05	6.6							
Ml. of Titrant A	5.8 5.4	7.8		5.5 5.6 5.4	7.4		5.0 5.1 4.9	7.6	
Averages	5.6	7.8		5.5			4.91		
460 + T	559.5			567			566.5		
Sample Vol. V	1.036								
P + p	23.62								
A - B	—	1.2		—	0.8		—	1.0	

TITRATED BY _____

$$SO_2 = \frac{(A-B)(N)(F)(460+T)(24)}{V(P+p)}$$

$$SO_2 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_2 = \boxed{429.4} \quad SO_3 = \boxed{9.28}$$

$$SO_3 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_2 @ 3\% O_2 = \underline{575}$$

$$SO_3 @ 3\% O_2 = \underline{11}$$

$$SO_x @ 3\% O_2 = \underline{526}$$

$$SO_2 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_2 = \boxed{429.9}$$

$$SO_3 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_3 = \boxed{6.31}$$

$$SO_2 @ 3\% O_2 = \underline{530}$$

$$SO_3 @ 3\% O_2 = \underline{8}$$

$$SO_x @ 3\% O_2 = \underline{538}$$

$$SO_2 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_2 = \boxed{375.2}$$

$$SO_3 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_3 = \boxed{7.83}$$

$$SO_2 @ 3\% O_2 = \underline{468}$$

$$SO_3 @ 3\% O_2 = \underline{10}$$

$$SO_x @ 3\% O_2 = \underline{478}$$

Local ABMA - SITE AMeter Correction = 1.036SOx DATA SHEETDate 10/29/77 Probe Location & Probe Length ESP OUTUnit # 1 Fuel Consolidation Coal Load 76%

Test Description: _____

Test No.	Box No.	Sample Time	Meter Temp. (T)	Meter (P) Press.	Meter Reading	(P) Baro. Press.	Port	Purge Time	O2
34D	1	16:49	54	-0-	0.000	23.62	4	17:12	6.4
			53		1.036			17:42	—
34E	3	17:15	46		0.000			17:43	6.7
		17:29	46		1.036			18:13	6.5
34F	2	17:34	46		0.000				6.8
		17:47	46		1.036				

SAMPLED BY _____

Test # 34DTest # 34ETest # 34F

	SO2	SO3	SOx	SO2	SO3	SOx	SO2	SO3	SOx
Normality N	.0141								
Dilution Factor F	10	1		10	1		10	1	
Blank B	0.4	5.152							
		6.7							
Averages									
Ml. of Titrant A	9.7	8.1		6.0	7.2		5.2	9.3	
	9.7			5.8			6.0		
	6.9			6.0			6.0		
Averages	8.76	8.1		5.93	7.2		5.73		
460 + T	513.5			506			506		
Sample Vol. v	1.036			1.03			1.036		
P + p	23.62								
A - B	.36	1.4		5.53	1.1		5.33	1.6	

TITRATED BY _____

$$SO_2 = \frac{(A-B)(N)(F)(460+T)(24)}{V(P+p)}$$

$$SO_2 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_2 = \boxed{593.7} \quad SO_3 = \boxed{9.94}$$

$$SO_3 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_2 @ 3\% O_2 = \underline{732}$$

$$SO_3 @ 3\% O_2 = \underline{12}$$

$$SOx @ 3\% O_2 = \underline{744}$$

$$SO_2 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_2 = \boxed{387.2}$$

$$SO_3 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_3 = \boxed{7.70}$$

$$SO_2 @ 3\% O_2 = \underline{484}$$

$$SO_3 @ 3\% O_2 = \underline{10}$$

$$SOx @ 3\% O_2 = \underline{494}$$

167

$$SO_2 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_2 = \boxed{373.2}$$

$$SO_3 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_3 = \boxed{11.20}$$

$$SO_2 @ 3\% O_2 = \underline{473}$$

$$SO_3 @ 3\% O_2 = \underline{14}$$

$$SOx @ 3\% O_2 = \underline{487}$$

Local ABMA-SITEAMeter correction ^{#1} 1.036
^{#2} 1.03

SOx DATA SHEET

Date 10-30-77 Probe Location & Probe Length 18" BLR OUTUnit # 1 Fuel Consolidated Coal Load 80%

Test Description: _____

Test No.	Box No.	Sample Time	Meter Temp. (T)	Meter (P) Press.	Meter Reading	(P) Baro. Press.	Port	Purge Time	O2
35A	1	13:55	97	-5-	0.000	23.62	4	14:17	6.0
		14:07	108		.000			14:48	
35B	2	14:25	65		0.000			14:51	5.85
		14:28	96		1.000			15:25	
35C	3	15:06	88		0.000			15:27	
		15:18	106		1.0			16:05*	6.0

SAMPLED BY _____

Test # 35ATest # 35BTest # 35C

* glow wire separated during purge

	SO2	SO3	SOx	SO2	SO3	SOx	SO2	SO3	SOx
Normality N	.0141								
Dilution Factor F	10	1		10	1		10	1	
Blank B	0.1	5.142							
		6.7							
Averages									
Ml. of Titrant A	4.3	7.6		4.8	7.4		4.6	7.5	
	4.6			4.6			4.7		
	4.4			4.6			4.8		
Averages	4.4	7.6		4.7			4.7	7.5	
460 + T	562.5			540.5					
Sample Vol. V	1.03			1.036			1.056		
P + p	23.62								
A - B	4.3	0.9		4.6	0.7		4.6	0.8	

TITRATED BY _____

$$SO_2 = \frac{(A-B)(N)(F)(460+T)(24)}{V(P+p)}$$

$$SO_2 = \frac{(4.3)(.0141)(10)(562.5)(24)}{(1.03)(23.62)}$$

$$SO_2 = \boxed{336.4} \quad SO_3 = \boxed{7.04}$$

$$SO_3 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_2 @ 3\% O_2 = \underline{404}$$

$$SO_3 @ 3\% O_2 = \underline{8}$$

$$SO_x @ 3\% O_2 = \underline{412}$$

$$SO_2 = \frac{(4.6)(.0141)(10)(540.5)(24)}{(1.036)(23.62)}$$

$$SO_2 = \boxed{343.8}$$

$$SO_3 = \frac{(0.7)(.0141)(1)(540.5)(24)}{(1.06)(23.62)}$$

$$SO_3 = \boxed{5.23}$$

$$SO_2 @ 3\% O_2 = \underline{408}$$

$$SO_3 @ 3\% O_2 = \underline{6}$$

$$SO_x @ 3\% O_2 = \underline{414}$$

$$SO_2 = \frac{(4.6)(.0141)(10)(55)(24)}{(1.0)(23.62)}$$

$$SO_2 = \boxed{347.7}$$

$$SO_3 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_3 = \boxed{6.14}$$

$$SO_2 @ 3\% O_2 = \underline{417}$$

$$SO_3 @ 3\% O_2 = \underline{7}$$

$$SO_x @ 3\% O_2 = \underline{424}$$

SOx DATA SHEETDate 10/30/77 Probe Location & Probe Length ESP OUTUnit # 1 Fuel CONSOLIDATION COAL Load _____

Test Description: _____

Test No.	Box No.	Sample Time	Meter Temp. (T)	Meter (P) Press.	Meter Reading	(P) Baro. Press.	Port	Purge Time	O2
35D	1	16:39	70	-0-	0.000	23.62	4		8.1
		16:54	53		1.030				-
35E	2	17:00	50		0.000				7.9
		17:14	44		1.030				7.9
35F	3	17:19	42		0.000				7.7
		17:32	39		1.030				7.7

SAMPLED BY _____

Test # 35DTest # 35ETest # 35F

	SO2	SO3	SOx	SO2	SO3	SOx	SO2	SO3	SOx
Normality N	.0141								
Dilution Factor F	10	1		10	1		10	1	
Blank B	0.2	SPike							
		6.7							
Averages		subtract spike x 2							
Ml. of Titrant A	4.0	13.4		4.2	7.1		4.3	7.0	
	4.1			4.2			4.4		
	4.3			4.3			4.3		
Averages	4.13			4.23			4.33		
460 + T	521.5			507			500.5		
Sample Vol. V	1.030								
P + p	23.62								
A - B	7.93	0		4.03	0.4		4.13	0.3	

TITRATED BY _____

$$SO_2 = \frac{(A-B)(N)(F)(460+T)(24)}{V(P+p)}$$

$$SO_2 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_2 = \boxed{285.3} \quad SO_3 = \boxed{0}$$

$$SO_3 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_2 @ 3\% O_2 = \underline{352}$$

$$SO_3 @ 3\% O_2 = \underline{0}$$

$$SO_x @ 3\% O_2 = \underline{352}$$

$$SO_2 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_2 = \boxed{214.4}$$

$$SO_3 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_3 = \boxed{2.82}$$

$$SO_2 @ 3\% O_2 = \underline{353}$$

$$SO_3 @ 3\% O_2 = \underline{4}$$

$$SO_x @ 3\% O_2 = \underline{357}$$

$$SO_2 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_2 = \boxed{287.8}$$

$$SO_3 = \frac{(\quad)(\quad)(\quad)(\quad)(24)}{(\quad)(\quad)}$$

$$SO_3 = \boxed{2.09}$$

$$SO_2 @ 3\% O_2 = \underline{355}$$

$$SO_3 @ 3\% O_2 = \underline{5}$$

$$SO_x @ 3\% O_2 = \underline{358}$$

SECTION 4.0
SPECIAL TESTS

	<u>PAGE</u>
4.1 MODIFIED SMOKE SPOT DATA SHEET	171
4.2 PARTICLE SIZE DISTRIBUTION - BRINK	172
- SASS CYCLONES	178
- BAHCO	182
- COULTER	185
4.3 CORROSION PROBE DATA SHEET AND LOG	188

KVB

SMOKE SPOT DATA SHEET

TEST SITE A - Boiler Outlet

TEST NO.	NO. PUMPS	READING	PARTICULATES lb/10 ⁶ BTU	COMBUSTIBLES %	COMBUSTIBLES lb/10 ⁶ BTU
21	1	3.0, 4.0	12.1830	72.1	8.7859
21	2	7.0, 6.0	12.1830	72.1	8.7859
22	1	6.0	16.7105	58.4	9.7589
22	2	7.5	16.7105	58.4	9.7589
23	1	2.5, 2.0	11.7238	43.7	5.1233
23	2	4.0, 4.0	11.7238	43.7	5.1233
24	1	2.5	8.4772	60.8	5.1511
24	2	4.0	8.4772	60.8	5.1511
26	1	8.0, 8.5	9.8190	52.5	5.1353
26	2	9.0, 9.0	9.8190	52.5	5.1353
28	1	30.5, 5.5	20.5734	65.7	13.5167
28	2	60.5, 5.0	20.5734	65.7	13.5167
29	1	10.1, 1.0	15.4111	56.8	8.1060
29	2	30.5, 1.0	15.4111	56.8	8.1060

KVB

BRINK CASCADE IMPACTOR DATA REDUCTION

TEST NO. 14 LOAD 72%
 TEST SITE A % O₂ 5.6
 TEST DATE 8-26-77 FUEL _____
 SAMPLE LOCATION Multiclone Outlet SPECIAL CONDITIONS AS FOUND

ρ_p - Density of particles 2.5 g/cm³ Vn - Dry gas volume 1.7 SCF
 μ - Viscosity of flue gas 2.57×10^{-4} poise Mn - Total particulate mass 25.2 mgm
 MW - Molecular wt. flue gas 29.47 g/g mole Cn - Total concentration .229 grains/SCF
 ΔP_I - Pressure drop across impactor 24.7 in H₂O I - Percent isokinetics 113 %
 Ps - Absolute stack pressure 23.54 in. Hg Vs - Gas velocity 42.82 ft/sec
 Ts - Absolute stack temperature 930 °R Dn - Nozzle diameter .076 in.
 Q - Actual flow rate at stack conditions .0809 ft³/min

Stage Number	CYCLONE	1	2	3	4	5	FINAL FILTER
Dj - Jet Diameter, cm	—	.2434	.1755	.1375	.0930	.0726	—
Fj - Press. factor, n.d.	—	.0210	.0273	.0395	.0903	.3277	—
D _{S,50} Stokes diameter, μ m	~ 7.0?	2.52	1.43	0.91	0.41	0.23	—
D _{A,50} Aerodynamic diameter, μ m	?	4.15	2.42	1.59	0.77	0.45	—
D _{AI,50} Aerodynamic impaction diameter, μ m	?	4.47	2.73	1.89	1.05	0.72	—
Mn - Particulate mass, mgm	14.5	5.4	3.2	3.4	0.3	0.2	0.2
% - Percent of Total	57.5	23.4	12.7	3.6	1.2	0.8	0.8
Cumulative percent	100.0	42.5	19.1	6.4	2.8	1.6	0.8
Cn - Concentration, grains/SCF	.1316	.0536	.0290	.0082	.0027	.0018	.0018
Cumulative concentration, grains/SCF	.2288	.0471	.0436	.0145	.0064	.0036	.0018

#15900

KVB

BRINK CASCADE IMPACTOR DATA SHEET

TEST NO. 14 LOAD 72%
 TEST SITE A % O₂ 5.6
 TEST DATE 8-26-77 FUEL _____
 SAMPLE LOCATION Multiclone Outlet SPECIAL CONDITIONS AS FOUND

GAS VELOCITY DETERMINATION

PITOT TUBE ΔP .30/.25/.215 BAROMETRIC PRESS in. Hg, P_{bar} 23.80
 GAS TEMP. °R, T_s 930 GAS STATIC PRESS in. H₂O 3.6
 PITOT CORRECTION FACTOR, C_p .837 GAS STATIC PRESS in. Hg abs., P_s 23.54
 MOLECULAR WT. FLUE GAS, MW 28 assumed

$$V_s = 85.48 C_p \left(\frac{T_s \Delta P}{P_s MW} \right)^{1/2} = \underline{46.55/42.49/39.41} \text{ ft/sec}$$

IMPACTOR FLOW RATE DETERMINATION

NOZZLE DIAMETER inches, D_n .076
 NOZZLE AREA ft², A_n 3.15×10^{-5} $A_n = \pi (D_n/24)^2$
 $Q_n = V_s A_n 60 = \underline{.0880/.0803/.0745} \text{ ft}^3/\text{min}$ at nozzle
 $Q_c = Q_n \sqrt{\frac{530}{T_s}} = \underline{.0664/.0606/.0562} \text{ ft}^3/\text{min}$ corrected to calibration conditions
 PRESSURE DROP ACROSS IMPACTOR FROM CALIBRATION CURVE 20.3/17.2/15.0 in. H₂O
 OPERATING VACUUM (corrected for static pressure of duct) 23.9/20.8/18.6 in. H₂O*

ISOKINETICS DETERMINATION

* actual operating vacuums were
 34.0/27.2/23.8 but could
 not be maintained because of
 leaks in Brink causing vacuum to
 continuously drop.

	SAMPLE TIME (θ)	METER READING (Vm)	METER TEMP (Tm)
INITIAL	5:04/5:10/5:35	0/0/0	88/88/89
FINAL	5:16/5:31/5:46	.6/.6/.5	—
Δ min	11.72/12.18/11.32	.6/.6/.5	548/548/549

$$I = \frac{1.667 T_s V_m P_{bar}}{\theta T_m V_s P_s A_n \left(1 - \frac{\%H_2O}{100}\right)} = \frac{110.1}{116.1} = 112.0$$

% H₂O = 9.3 (assumed)

KVB

BRINK CASCADE IMPACTOR LAB WORKSHEET

TEST No. 14 LOCATION A
 TEST DATE 8-26-77 ENGINEER R.A.P.
 TEST DESCRIPTION Multichone Outlet

PRE TEST WEIGHTS (GRAMS)

PLATE NO.		CYCLONE	1	2	3	4	5	FINAL FILTER
DATE WT.								+ SCREEN
TARE WT.	1	0.3988	3.4092	3.2676	3.4934	3.4609	3.2983	2.0068
	2		3.4092	3.2675	3.4933	3.4609	3.2983	2.0068
	3		3.4091	3.2674	3.4932	3.4608	3.2983	2.0067
	4							
AVERAGE		0.3988	3.4092	3.2675	3.4933	3.4609	3.2983	2.0068

POST TEST WEIGHTS (GRAMS)

DATE WT.								
GROSS WT.	1	0.4133	3.4151	3.2707	3.4942	3.4612	3.2985	2.0070
	2							
	3							
	4							
AVERAGE		0.4133	3.4151	3.2707	3.4942	3.4612	3.2985	2.0070

NET TEST RESULTS (MG/M)

NET WT.	14.5	5.9	3.2	0.9	0.3	0.2	0.2
PERCENT	57.5	23.4	12.7	3.6	1.2	0.8	0.8

TOTAL NET WEIGHT 25.2 mgm

KVB

BRINK CASCADE IMPACTOR DATA REDUCTION

TEST NO. 19 LOAD 44%
 TEST SITE A % O₂ 6.8
 TEST DATE 9-12-77 FUEL _____
 SAMPLE LOCATION Multisone Outlet SPECIAL CONDITIONS AS FOUND

Pp - Density of particles 2.5 g/cm³ Vn - Dry gas volume NA SCF
 μ - Viscosity of flue gas 2.37x10⁻⁴ poise Mn - Total particulate mass 21.7 mgm
 MW - Molecular wt. flue gas 29.18 g/g mole Cn - Total concentration NA grains/SCF
 ΔP_I - Pressure drop across impactor 11.5 in H₂O I - Percent isokinetics NA %
 Ps - Absolute stack pressure 23.63 in. Hg Vs - Gas velocity 25.49 ft/sec
 Ts - Absolute stack temperature 840 °R Dn - Nozzle diameter .077 in.
 Q - Actual flow rate at stack conditions .0495 ft³/min

Stage Number	CYCLONE	1	2	3	4	5	FINAL FILTER
Dj - Jet Diameter, cm	—	.2434	.1755	.1375	.0430	.0726	—
Fj - Press. factor, n.d.	—	.0210	.0273	.0395	.0903	.3277	—
Ds, $\overline{50}$ Stokes diameter, μm	—	3.22	1.87	1.22	0.59	0.35	—
D _{A, $\overline{50}$} Aerodynamic diameter, μm	?	5.24	3.10	2.07	1.05	0.65	—
D _{AI, $\overline{50}$} Aerodynamic impaction diameter, μm	?	5.51	3.37	2.33	1.30	0.89	—
Mn - Particulate mass, mgm	12.6	3.3	3.6	1.3	0.5	0.2	0.2
% - Percent of Total	52.1	15.2	10.5	5.3	2.3	0.9	0.9
Cumulative percent	100.0	41.9	23.7	10.1	4.1	1.8	0.4
Cn - Concentration, grains/SCF	NA						
Cumulative concentration, grains/SCF	NA						

#15900

KVB

BRINK CASCADE IMPACTOR DATA SHEET

TEST NO. 19 LOAD 44.7
 TEST SITE A % O₂ 6.8
 TEST DATE 9-12-77 FUEL _____
 SAMPLE LOCATION Multiclone Outlet SPECIAL CONDITIONS AS FOUND

GAS VELOCITY DETERMINATION

PITOT TUBE ΔP .10 BAROMETRIC PRESS in. Hg, P_{bar} 23.78
 GAS TEMP. °R, T_s 840 GAS STATIC PRESS in. H₂O -2.0
 PITOT CORRECTION FACTOR, C_p .837 GAS STATIC PRESS in. Hg abs. P_s 23.63
 MOLECULAR WT. FLUE GAS, MW 28 assumed

$$V_s = 85.48 C_p \left(\frac{T_s \Delta P}{P_s MW} \right)^{1/2} = \underline{25.49} \text{ ft/sec}$$

IMPACTOR FLOW RATE DETERMINATION

NOZZLE DIAMETER inches, D_n .077
 NOZZLE AREA ft², A_n 3.234×10^{-5}

$$A_n = \pi (D_n/24)^2$$

$$Q_n = V_s A_n 60 = \underline{.0475} \text{ ft}^3/\text{min at nozzle}$$

$$Q_c = Q_n \sqrt{\frac{530}{T_s}} = \underline{.0393} \text{ ft}^3/\text{min corrected to calibration conditions}$$

PRESSURE DROP ACROSS IMPACTOR FROM CALIBRATION CURVE 7.6 in. H₂O

OPERATING VACUUM (corrected for static pressure of duct) 9.6 * in. H₂O

ISOKINETICS DETERMINATION

* Brink was operated at a ΔP of 11.5 in. H₂O.

	SAMPLE TIME (θ)	METER READING (V_m)	METER TEMP (T_m)
INITIAL	—	0	117
FINAL	—	.907	
Δ	15.117 min	out of service	57.7 °R

$$I = \frac{1.667 T_s V_m P_{bar}}{\theta T_m V_s P_s A_n \left(1 - \frac{\%H_2O}{100}\right)} = \underline{NA}^+ \%$$

+ Dry gas meter inoperative

KVB

BRINK CASCADE IMPACTOR LAB WORKSHEET

TEST No. 19 LOCATION A
 TEST DATE 12 Sep 77 ENGINEER R.A.P.
 TEST DESCRIPTION Multiclone Outlet

PRE TEST WEIGHTS (GRAMS)

PLATE NO.	CYCLONE	1	2	3	4	5	FINAL FILTER
DATE WT.		7-9-77					
TARE WT.	1	0.4113	3.4090	3.2677	3.4936	3.4603	3.2973
	2		3.4091	3.2676	3.4935	3.4603	3.2972
	3		3.4091	3.2676	3.4936	3.4603	3.2973
	4						
AVERAGE		0.4113	3.4091	3.2676	3.4936	3.4603	3.2973

POST TEST WEIGHTS (GRAMS)

DATE WT.							
GROSS WT.	1	0.4239	3.4124	3.2712	3.4449	3.4608	3.2975
	2						
	3						
	4						
AVERAGE		0.4239	3.4124	3.2712	3.4449	3.4608	3.2975

NET TEST RESULTS (MGM)

NET WT.	12.6	3.3	3.6	1.3	0.5	0.2	0.2
PERCENT	58.1	15.2	16.6	6.0	2.3	0.9	0.7

TOTAL NET WEIGHT 21.7 mgm

177

#15900

SASS GRAVIMETRICS

TEST SITE A

TEST #27

<u>Sample</u>	<u>Pretest Weight (gms)</u>	<u>Post Test Weight (gms)</u>	<u>Net Weight (gms)</u>
LPE #1	23.9247	50.6233	
Probe + 10 microns	23.9248	50.6233	
Cyclone Solids	<u>23.9248</u>	<u>50.6237</u>	
	23.9248	50.6237	26.6986
LPE #2	23.9383	25.4696	
3 microns cyclone	23.9383	25.4696	
Solids	<u>23.9383</u>	<u>25.4698</u>	
	23.9383	25.4697	1.5313
LPE #3	23.4086	24.1139	
1 micron cyclone	23.4086	24.1142	
Solids	<u>23.4087</u>	<u>24.1144</u>	
	23.4086	24.1142	0.7056
Filter #24	1.2846	1.6239	
	1.2842	1.6241	
	<u>1.2841</u>	<u>1.6242</u>	
	1.2843	1.6241	0.3398
Filter #25	1.2936	1.6701	
	1.2935	1.6702	
	<u>1.2935</u>	<u>1.6702</u>	
	1.2935	1.6702	0.3767

TEST 27 BOILER OUT:

	<u>Net Weight, grams</u>	
10 microns	26.6986	
3 microns	1.5313	9.96% below 10 microns
1 micron	0.7056	4.80% below 3 microns
filter	<u>0.7165</u>	2.42% below 1 micron
TOTAL	29.6520	

SITE A - SASS GRAVIMETRICS

TEST 34 BOILER OUT:

	<u>Net Weight, grams</u>	
10 microns	202.57333	
3 microns	14.00929	9.32% below 10 microns
1 micron	3.23020	3.05% below 3 microns
filter	<u>3.57714</u>	1.60% below 1 micron
Total	223.38996	

TEST 35 BOILER OUT:

	<u>Net Weight, grams</u>	
10 microns	42.24569	
3 microns	11.34526	24.06% below 10 microns
1 micron	1.54490	3.66% below 3 microns
filter	<u>0.49162</u>	0.88% below 1 micron
Total	55.62747	

TEST 34 ESP OUT:

	<u>Net Weight, grams</u>	
10 microns	0.27726	
3 microns	0.19750	75.52% below 10 microns
1 micron	0.43368	58.09% below 3 microns
filter	<u>0.22424</u>	19.80% below 1 micron
Total	1.13268	

TEST 35 ESP OUT:

	<u>Net Weight, grams</u>	
10 microns	0.05091	
3 microns	0.05588	82.18% below 10 microns
1 micron	0.11949	62.62% below 3 microns
filter	<u>0.05940</u>	20.79% below 1 micron
Total	0.28568	

SASS FILTERS

PARTICULATE LAB WORKSHEET

Cyclone Containers

TEST NO. 4C (Inlet, Outlet)

LOCATION ABMA-SITE A

Date 11-11-77

Box No. _____

Eng. _____

Test Description _____

Dry Gas Meter Vol (ft³)

Final _____

Initial _____

Δ DgV _____

Final

Initial

Δ Vlc

Impinger Water Vol (ml)

1	2	3	Total

CONTENT						
BOTTLE NO.	<u>10M cyclone</u>	<u>3M cyclone</u>	<u>1M cyclone</u>	<u>Filter #30</u>	<u>Filter #31</u>	<u>FILTER #32</u>
BEAKER NO.	<u>1</u>	<u>2</u>	<u>3</u>			
DATE WT.	<u>11-12-77</u>	<u>11-12-77</u>	<u>11-12-77</u>	<u>11-12-77</u>	<u>11-12-77</u>	
TARE WT.	1	2	3			
	23.9677	23.6245	23.9025	1.2508	1.2521	1.2575
	2	23.9678	23.6246	23.9022	1.2511	1.2525
	3	23.9678	23.6246	23.9023	1.2512	1.2525
	4	—	—	—	—	1.2506
AVG.	23.9678	23.6246	23.9023			1.2508

POST TEST WTS.

1	48.2352	31.6816	26.9661	2.2129	2.0336	
2	48.2348	31.6812	26.9659	2.2129	2.0337	
3	48.2347	31.6813	26.9658	2.2124	2.0336	
4	—	—	—	—	—	
AVG.	48.2349	31.6814	26.9659	2.2126	2.0336	
Δ WT.	24.2671	8.0568	3.0636	0.9614	0.7811	

Δ Vlc = _____ ml

LOAD _____ klb/hr

Δ DgV = _____ ft³

O₂ _____ %

Δ Mn _____ mgm

REMARKS: _____

Filter #33

1.2589

1.2589

1.2591

M. YAD₂ Condensate

SASS - CONTAINERS — TEST #40

— 10μ cyclone —

PARTICULATE LAB WORKSHEET

TEST NO. 40 (Inlet, Outlet)

LOCATION ABMA - SITE A

Date 11-11-77

Box No. _____

Eng. _____

Test Description _____

Dry Gas Meter Vol (ft³)

Final _____

Initial _____

Δ DgV _____

Impinger Water Vol (ml)

1	2	3	Total
Final			
Initial			
Δ Vlc			

CONTENT	H ₂ O RINSE	ACETONE RINSE	DRY FLASK	FILTER NO.	BLANK NO.
BOTTLE NO.	10μ cyclone	10μ cyclone	10μ cyclone	10μ cyclone	10μ cyclone
BEAKER NO.	4	5	6	9	10
DATE WT.	11-12-77	11-12-77	11-12-77	11-12-77	11-12-77
TARE WT.	1	2	3	4	5
	23.9057	23.6372	23.3062	23.7069	24.0360
	2	23.9062	23.6377	23.3068	23.7063
	24.0359				
	3	23.9063	23.6376	23.3068	23.7063
	24.0358				
	4	—	—	—	—
AVG.	23.9061	23.6375	23.3066	23.7065	NOT

POST TEST WTS.

1	55.9844	52.4588	50.1788	62.3077	USED
2	55.9841	52.4585	50.1784	62.3075	
3	55.9841	52.4582	50.1784	62.3074	
4	—	—	—	—	
AVG.	55.9842	52.4585	50.1785	62.3075	
Δ WT.	32.0781	28.8210	26.8719	38.6010	

Δ Vlc = _____ ml

LOAD _____ klb/hr

Δ DgV = _____ ft³

O₂ _____ %

Δ Mn _____ mgm

REMARKS: _____

10μ cyclone — 150.6391
 3μ " — 8.0568
 1μ " — 3.0636
 161.7595

KVB, Incorporated
 Minneapolis, MN
 ES-0552 5299-01
 December 5, 1977

Sample No.	<u>K-22126</u>	<u>K-22127</u>
Sample Description	Ash Sample Test 31 ABMA Program	Multicone Ash Sample Test 32 Boiler A
Bahco Particle <u>Size Determination</u>		
% Through #100 (149 Microns)	35.3	28.9
Results: Terminal <u>Velocity(In/Min.)</u>	<u>Diameter</u> <u>(Microns)</u> <u>% Smaller</u>	<u>Diameter</u> <u>(Microns)</u> <u>% Smaller</u>
112.	25. 13.2	27. 22.8
79.0	21. 11.4	22. 21.0
31.0	13. 8.0	14. 15.3
12.3	8.3 5.6	8.8 8.5
4.15	4.8 3.9	5.1 4.0
0.96	2.3 1.6	2.5 1.4
0.35	1.4 0.6	1.5 0.5
Density, gms/cc (On #100 Mesh Material Only)	2.47	2.20

SAMPLE IDENTIFICATION

ABMA Program

SAMPLE NO.

K-22126

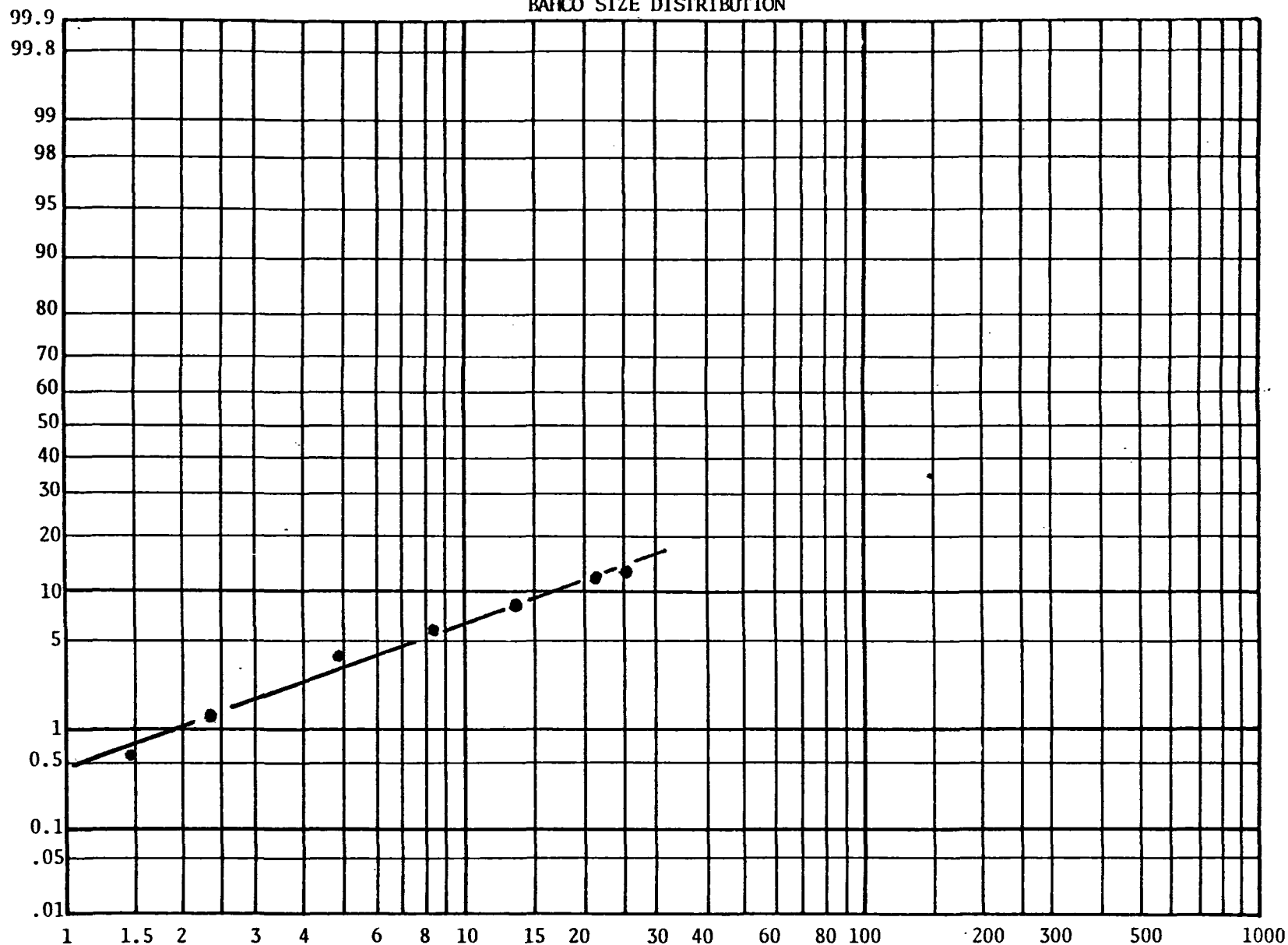
TEST #31, Ash Sample

CHARGE NO.

5299-01

BAHCO SIZE DISTRIBUTION

% SMALLER THAN STATED SIZE



EQUIVALENT PARTICLE DIAMETER - MICRONS

100m DENSITY 2.47 g/cc

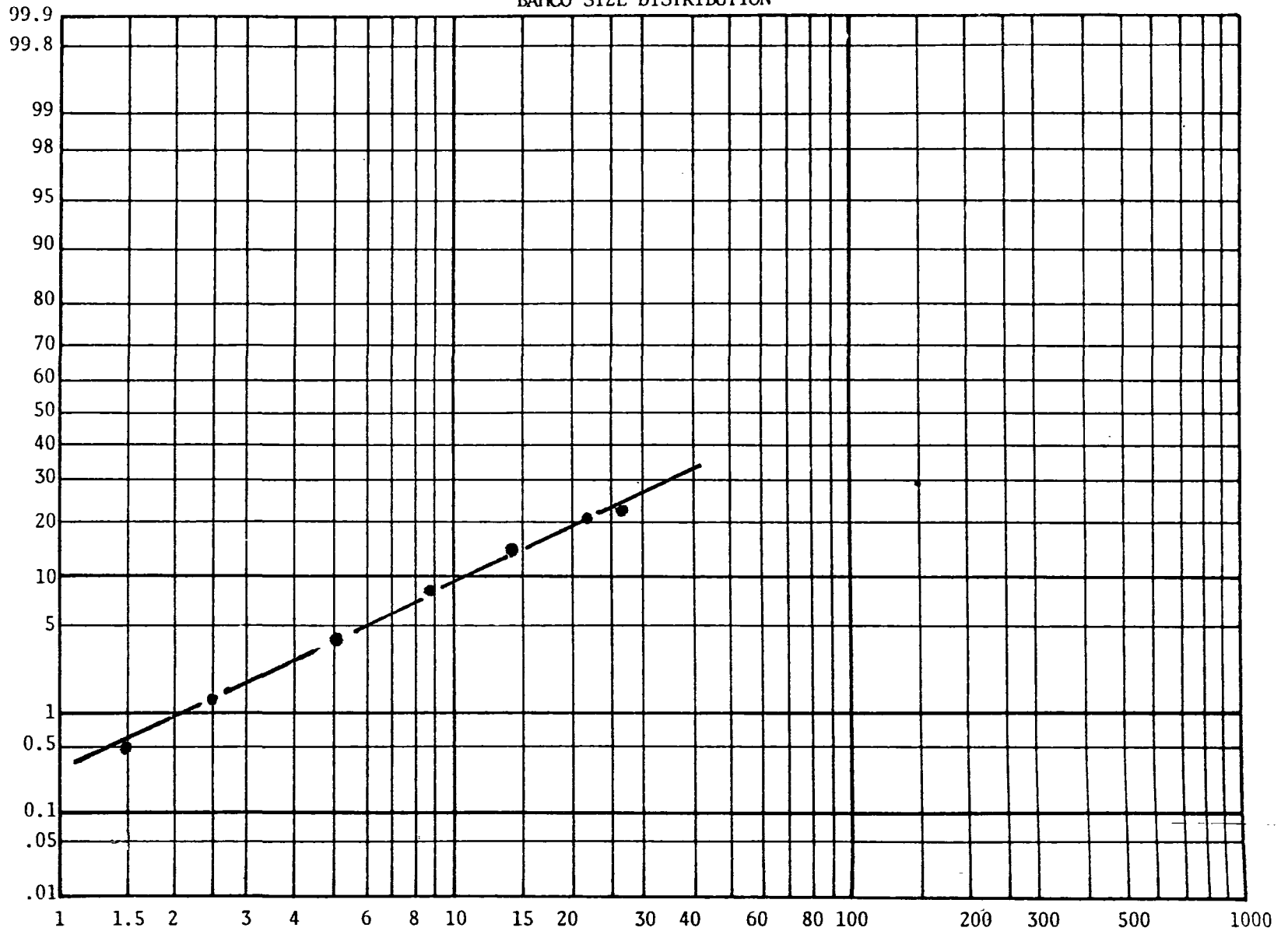
SAMPLE IDENTIFICATION MULTICONE Ash Sample
TEST 32, Boiler A

SAMPLE NO. K-22127
CHARGE NO. 5299-01

BAHCO SIZE DISTRIBUTION

181

% SMALLER THAN STATED SIZE



EQUIVALENT PARTICLE DIAMETER - MICRONS

100m DENSITY 2.20 g/cc



COULTER COUNTER®

Worksheet

SAMPLE

ELECTROLYTE

Isoton

DISPERSANT

EQUIPMENT TA II, sieves

SEIAL

Aper.
Dia.

Ser.
No.

CALIBRATION
DATA

Part.
Dia.

W

± 1 A

A

ORGANIZATION

K.V.B.

560

35932

MICROS.

42.87

8

3.2

143.3

OPERATOR

M.B.

DATE

12/14/77

± 1 A

3.2

CALIB. A

172.5

APERTURE DIA.

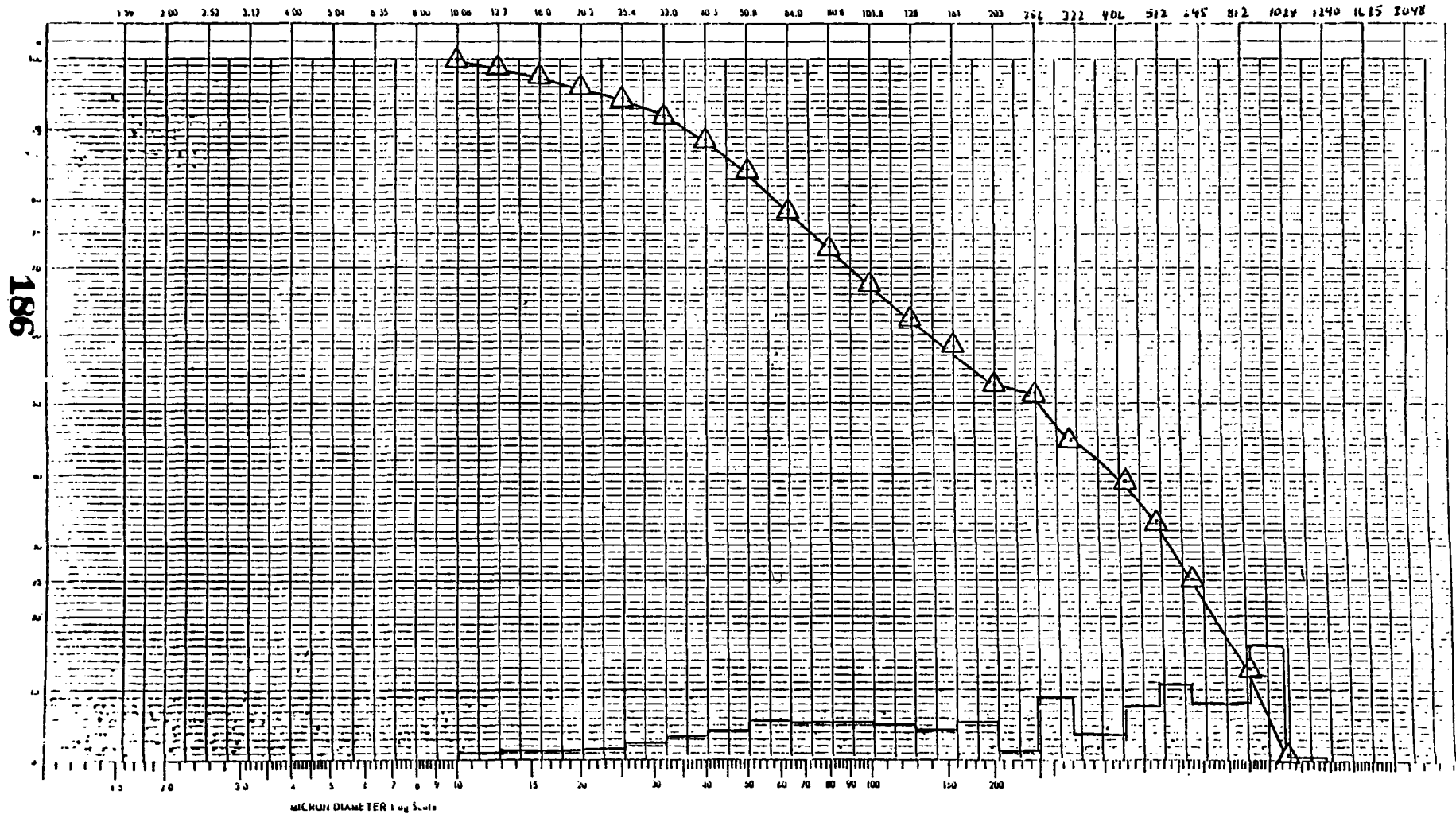
560

SAMPLE DATA

Geometric Mean μ^3	Volume μ^3	Diameter μ	Channel (W)		Test 31		Test 32		
			Relative Channel width x	Dif. wt. % / x	Dif wt %	Cum wt %	Dif wt %/ x	Dif wt %	Cum wt %
.0231	.01636	.315							
.0462	.03272	.397							
.0925	.06545	.500							
.1851	.1309	.630							
.3702	.2618	.794							
.7405	.5236	1.00							
1.481	1.047	1.26							
2.962	2.094	1.59							
5.924	4.189	2.00							
11.85	8.378	2.52							
23.70	16.76	3.17							
47.39	33.51	4.00							
94.78	67.02	5.04							
189.6	134.0	6.35							
379.1	268.1	8.00							
758.3	536.2	10.08	1	1.1	1.1	100.0	1.9	1.9	100.0
1516.	1072.	12.7	1	1.3	1.3	98.9	2.4	2.4	98.1
3033.	2145.	16.0	1	1.3	1.3	97.6	2.7	2.7	95.7
6066.	4289.	20.2	1	1.7	1.7	96.3	3.2	3.2	93.0
12.13 x 10 ³	8579.	25.4	1	2.5	2.5	94.6	3.7	3.7	89.8
24.27 x 10 ³	17.16 x 10 ³	32.0	1	3.5	3.5	92.1	3.5	3.5	86.1
48.54 x 10 ³	34.31 x 10 ³	40.3	1	4.3	4.3	88.6	2.9	2.9	82.6
97.18 x 10 ³	68.63 x 10 ³	50.8	1	5.8	5.8	84.3	2.3	2.3	79.7
194.4 x 10 ³	137.3 x 10 ³	64.0	1	5.4	5.4	78.5	2.2	2.2	77.4
388.7 x 10 ³	274.5 x 10 ³	80.6	1	5.4	5.4	73.1	1.8	1.8	75.2
777.4 x 10 ³	549.0 x 10 ³	101.6	1	5.1	5.1	67.7	1.4	1.4	73.4
1.555 x 10 ⁶	1.098 x 10 ⁶	128.	1	4.3	4.3	62.6	.4	.4	72.0
3.109 x 10 ⁶	2.196 x 10 ⁶	161.	1	5.5	5.5	58.3	0	0	71.6
6.219 x 10 ⁶	4.392 x 10 ⁶	203.	1	1.3	1.3	52.8	0	0	71.6
60 mesh	250		.75	8.9	6.7	51.5	2.1	1.6	71.6
50	300		1.5	3.8	5.7	44.8	1.9	2.8	70.0
40	420		.75	7.7	5.8	39.1	4.3	3.2	67.2
35	500		.75	10.8	8.1	33.3	7.9	5.9	64.0
30	595		1.5	8.2	12.3	25.2	8.0	12.0	58.1
20	840		.75	16.0	12.0	12.9	16.0	12.0	46.1
18	1000		2.25	.4	.9	.9	13.4	30.1	34.1
12	1600						4.0	4.0	4.0
10	2000								

2837A

COULTER COUNTER* Model T & TA		PARTICLE SIZE ANALYSIS		COULTER ELECTRONICS INC. 374 W 40 ST. HALEAT FLA 33016	
ORGANIZATION	KVB INCORPORATED	$L = 4 \sqrt{\frac{2}{\pi}}$ FOR MODEL T		$\frac{A_2}{A_1} = \left(\frac{d_2}{d_1}\right)^3$ when $W_2 = W_1$ FOR MODEL TA	
OPERATOR	M.B.			SAMPLE SETTINGS	
EQUIPMENT	TA II, sieves	APER. SIZE	SERIAL	PART DIA.	W
SAMPLE	ELECTROLYTE Isoton	560	35932	43	8
DISPERSANT		MICROSPHERES		3.2	143
Test 31				43	8
				3.2	172



28376

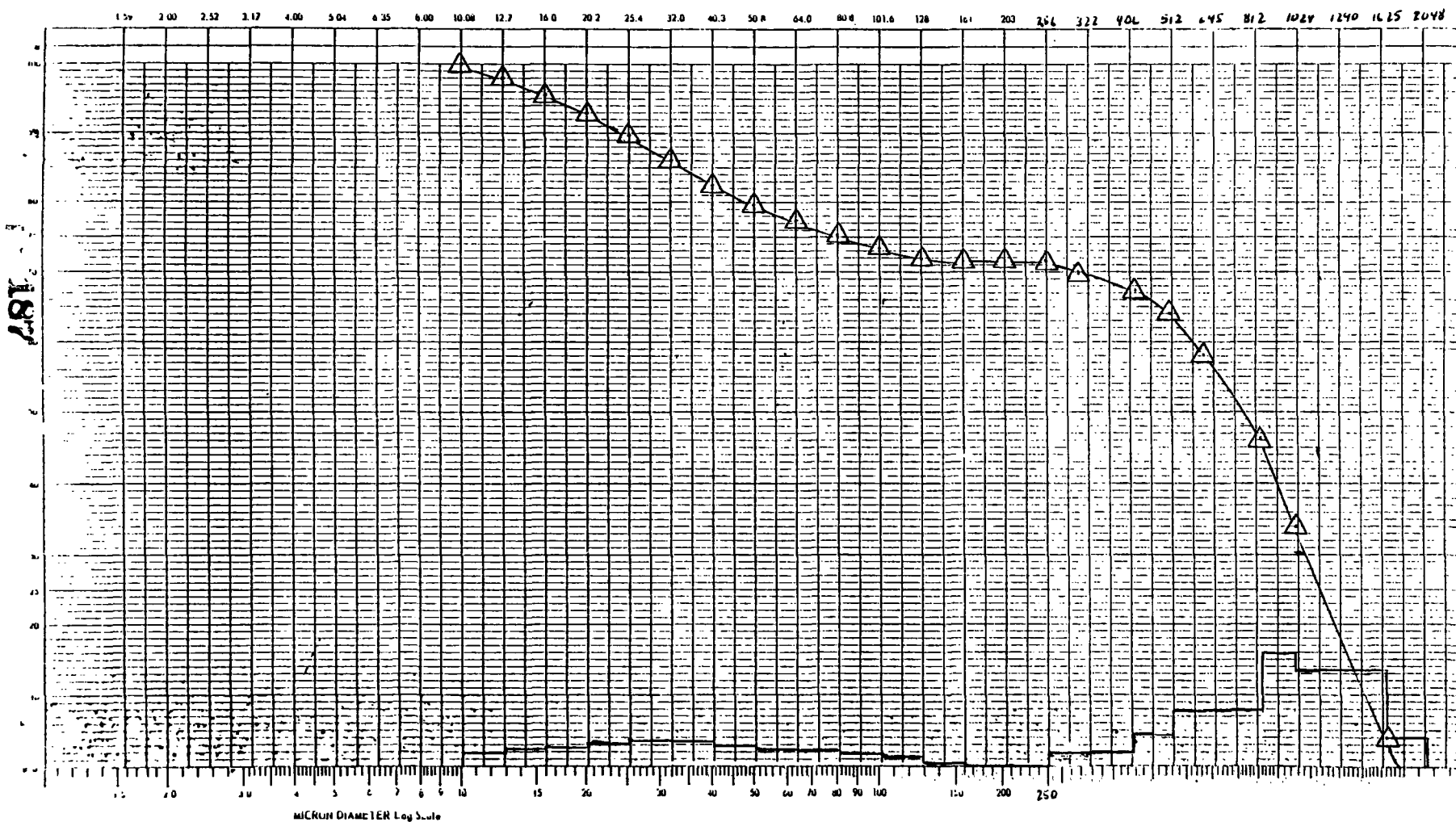


COULTER COUNTER® Model T & TA

PARTICLE SIZE ANALYSIS

.15 - 200 μ
1 PERCENTCOULTER ELECTRONICS INC.
590 W 20 ST.
MILWAUKEE, WIS. 53210

ORGANIZATION KVB INCORPORATED	$L = d \sqrt{\frac{2}{\pi}}$ FOR MODEL T		$\frac{\Delta Z}{\Delta I} = \left(\frac{d}{d_1}\right)^3$ when $W_2 = W_1$		$\frac{\Delta Z}{\Delta I} = \left(\frac{d_1}{d_2}\right)^3$ when $W_2 = W_1$		SAMPLE SETTINGS			
OPERATOR M.B.	APER. SIZE	SERIAL	PART DIA.	#	1/4	A	DIA.	W	± 1A	A
EQUIPMENT TA II, sieves	560	35932	43	8	3.2	143	43	8	3.2	172
SAMPLE Test 32	DISPERSANT									



KVB

CORROSION PROBE DATA SHEET

SITE A DATE IN 8/8/77
 PROBE PLACEMENT Consecutive Section
 COAL Stansbury, Kemmerer, Colorado

COUPON #	TARE WT, GM	DATE	FINAL WT, GM	WT LOSS, MG	DATE
19	31.1125		31.0487	(14 days)	9/11/77
	31.1127		31.0487	(4.6 mg/day)	
	AVG. 31.1126		31.0487	63.9	
20	31.5115	31.4487	31.2268	(57 days)	11/14/77
	31.5115	31.4488	31.2268	(11 mg/day)	
	AVG. 31.5115	31.4486	31.4487	62.8	
21	30.4891		30.3962	(45 days)	9/28/77
	30.4889		30.3966	(2.1 mg/day)	
	AVG. 30.4891		30.3963	92.8	
22			30.9872	(14 days)	9/11/77
			30.9875	(2.2 mg/day)	
	AVG. 31.0779		30.9875	30.4	
23	30.9789		30.8780	(45 days)	9/28/77
	30.9793		30.8779	(2.2 mg/day)	
	AVG. 30.9791		30.8778	101.2	
24	31.2705		31.2304	(80 days)	11/14/77
	31.2705		31.2304	(1.3 mg/day)	
	AVG. 31.2705		31.2303	102.9	
25	31.0752		30.9379	(57 days)	11/14/77
	31.0754		30.9379	(2.41 mg/day)	
	AVG. 31.0753		30.9381	137.3	
26	31.2690		31.2268	(80 days)	11/14/77
	31.2690		31.2268	(.53 mg/day)	
	AVG. 31.2690		31.2267	42.2	
27	30.9079		30.7798	(32 days)	11/14/77
	30.9081		30.7798	(4.0 mg/day)	
	AVG. 30.9080		30.7799	128.2	

KVB

CORROSION PROBE DATA SHEET

SITE ADATE IN 8-8-77PROBE PLACEMENT CONVECTIVE SECTIONCOAL STANSBURY, Kemmerer, CONSOLIDATION

COUPON #	TARE WT, GM	DATE	FINAL WT, GM	WT LOSS, MG	DATE
29	31.3462		31.1176	(32 days) (7.1 mg/day)	11/14/77
	31.3465		31.1177		
			31.1177		
	AVG. 31.3464		31.1177	228.7	
30	31.3664		31.3371	(80 days) (.4 mg/day)	Blank
	31.3663		31.3372		
			31.3371		
	AVG. 31.3664		31.3371	29.3	
31	30.7567				
	30.7566				
	AVG. 30.7566				
32	31.3238				
	31.3236				
	AVG. 31.3237				
33	31.3225				
	31.3225				
	AVG. 31.3225				
34					
	AVG. 31.1839				
35	30.4890				
	30.4892				
	AVG. 30.4891				
36	31.2538				
	31.2536				
	AVG. 31.2537				
37					
	AVG. 30.5743				

Corrosion Coupon Locations ABMA - Site A

1st day

19 IN 8/8/77
OUT 8/22/77
25 IN 9/1/77
OUT 10/27/77
IN
OUT

22 IN 8/8/77
OUT 8/22/77
20 IN 9/1/77
OUT 10/27/77
IN
OUT

14 days

45 days

21 IN 8/8/77
OUT 9/22/77
27 IN 9/25/77
OUT 10/27/77
IN
OUT

24 IN 8/8/77
OUT 10/27/77
IN
OUT
IN
OUT

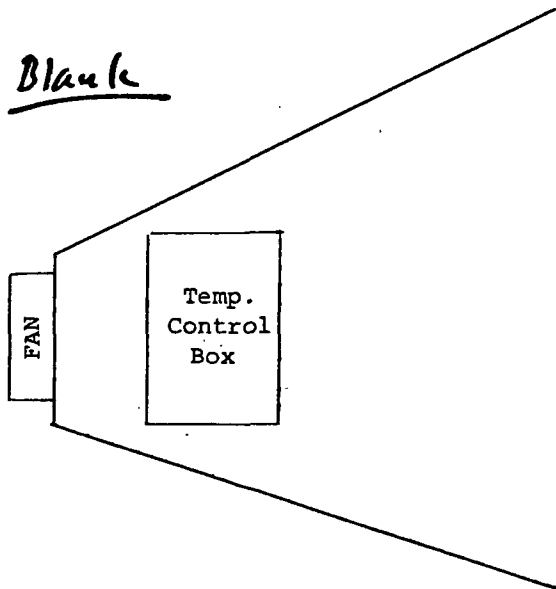
75 days

23 IN 8/8/77
OUT 9/22/77
29 IN 9/25/77
OUT 10/27/77
IN
OUT

26 IN 8/8/77
OUT 10/27/77
IN
OUT
IN
OUT

500

#30 - Blank



5th integrator

8/8/77 ~ 268370
8/22/77 ~ 287130
9/1/77 ~ 302630
10/27/77 ~ 383660
9/22/77 ~ 332670
9/25/77 ~ 338200

CORROSION PROBE LOGSITE A unit 1DATE IN Aug 8, 77 @ 3:30 pmPROBE PLACEMENT Convective SectionCOAL Stansbury, Kemmerer, Colorado

DATE	PROBE TEMP.	PROBE VAC. 11/20	BOILER LOAD	NOTES
8/8/77	650°F	-10 in Hg	140,000 ± 25,00	Installed @ 3:30 pm Convective Section
8/9/77	750°F	-7.5 in Hg	180,000	Fan on 100%
8/11/77	830°F	-7.5 "Hg	"	"
8/22/77	770°F	-7.5 "Hg	"	Probe Removed from furnace
8/25/77				T/C Broken at tip
9/25/77				530 ml Dowtherm Removed
				Coil #22 & #19 removed
				Installed #20 & #25
8/29/77	7900°F	-10 "Hg	180,000	T/C rewelded back on tip
				Leak checked at 40 psi. 550 ml
				Dowtherm added & reinsulated
				Reinstalled in convective sect.
				Probe overheated, Removed
9/1/77	700°F	-10 in Hg	200,000	Rewelded T/C into groove
				in Probe Tip. Reinsulated &
				reinstalled probe. Seems to
				work well w/ new T/C weld
				Fan making noise
9/2/77	700°F	-10 in Hg	200,000	Fan making noise but probe works
9/9/77	750°F	"	240,000	Fan failed over Holiday but
				Probe <u>did not</u> overheat
				fan replaced

CORROSION PROBE LOG

SITE A DATE IN 8-8-77
 PROBE PLACEMENT CONVECTIVE SECTION
 COAL STANSBURY, KEMMERER, CONSOLIDATION

DATE	PROBE TEMP.	PROBE VAC. "H ₂ O	BOILER LOAD	NOTES
9/11/77	610°F	-10" H ₂	180,000	New Feen working well
9/22/77	700°F	-10" H ₂		Probe removed for coupon change
9/25/77	610°F	-10" H ₂		replaced coupons 21+23 with coupons 27+29, 28 was scrapped because of manufacturing flaws. 550 ml DowTherm recovered
9/26/77	600°F	-10" H ₂		Site A boiler #1 was taken off line for repairs. extension cord removed to power SASS meter box. Controlled at 600°F while boiler winding down
10/2/77				Boiler started on line again
10/27/77	720°F	-10" H ₂	97%	from checking frequently probe ran without difficulty and maintained temperature range easily
				probe removed permanently from site A

SECTION 5.0
FUEL AND ASH ANALYSIS

	<u>PAGE</u>
5.1 LIST OF COAL AND ASH SAMPLES ANALYZED	194
5.2 COMMERCIAL TESTING ANALYSIS	195
5.3 COMBUSTIBLES ANALYSIS	244
5.4 COAL SIEVE ANALYSIS	247

LIST OF COAL AND ASH SAMPLES ANALYZED
ABMA - TEST SITE A

Test No.	Coal & Test*	Coal Sample [†]	Bottom Ash Sample	Multiclone Ash Sample
1	S - SOx	Prox, Ult, Sulfur Forms	--	--
3	S - Part	--	--	--
4	S - Part, Brink	--	--	--
5	S - Part	Prox	--	--
6	S - Part	--	--	--
8	S - SOx	Prox	% Sulfur	--
9	S - SOx	Prox	% Sulfur	--
10	S - Part	Prox, Ult, Min, Fus	--	--
12	S - SOx	Prox	--	--
14	S - Part, Brink	Prox	% Combustibles	--
15	S - Part	Prox	--	--
16	S - Part	Prox	% Combustibles	--
17	SK - Part	Prox	% Combustibles	--
18	SK - SOx	Prox	% Sulfur	--
19	S - Brink	Prox	--	--
20	K - SOx, Brink	--	--	--
21	K - Part	Prox	--	% Combustibles
22	K - Part	Prox	--	--
23	K - Part	Prox, Ult, Min	% Combustibles	--
24	K - Part	Prox, Fus	% Combustibles	% Combustibles
26A	K - Part	Prox	% Combustibles	% Combustibles
26B	K - Part	Prox	% Combustibles	% Combustibles
27	K - SASS	Prox, Ult, Min	X	X
28	K - Part	Prox	--	% Combustibles
29	K - Part	Prox, Ult, Fus	% Combustibles	% Combustibles
30	K - Brink	Prox	--	--
34	C - SASS, Part, SOx	Prox	% Comb, % Sulfur	% Comb, % Sulfur
35	C - SASS, Part, SOx	Prox, Ult, Min, Fus	% Comb, % Sulfur	% Comb, % Sulfur
36	C - Part	Prox	--	% Combustibles
37	C - Part	Prox	--	--
38	C - Part	Prox	% Combustibles	% Combustibles
39	C - Part	Prox	% Combustibles	% Combustibles
40	K - SASS	Prox, Ult, Min	X	X

* S - Stansbury Coal Co. Prox - Proximate Analysis
 K - Kemmerer Coal Co. Ult - Ultimate Analysis
 SK - Blend of Stansbury & Kemmerer Min - Mineral Analysis
 C - Consolidation Coal Co. Fus - Ash Fusion Temperatures
 Part - Particulate Loading X - Sample Held for Future Analysis
 SOx - Sulfur Oxides -- - No Sample Obtained
 Brink - Brink Cascade Impactor
 SASS - Source Assessment Sampling System

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 328 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
18130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473



OFFICE TEL. (312) 264-1173

Aug. 30, 1977

KVB, INC.
600 S. County Road 18
Minneapolis, MN 55426

Kind of sample
reported to us -----

Sample identification
by
KVB, Inc.

Coal Sample
TEST SITE A
8/8/77

Sample taken at -----

Taken from Conveyor belt,
not associated with test

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. 71-5193

PROXIMATE ANALYSIS

	As Rec'd	Dry
% Moisture	14.21	xxxxx
% Ash	7.00	8.16
% Volatile	33.96	39.58
% Fixed Carbon	44.83	52.26
	100.00	100.00
Btu	10365	12082
% Sulfur	1.05	1.22

ULTIMATE ANALYSIS

	As Rec'd	Dry
% Moisture	14.21	xxxxx
% Carbon	60.64	70.68
% Hydrogen	4.24	4.94
% Nitrogen	1.01	1.18
% Chlorine	0.00	0.00
% Sulfur	1.05	1.22
% Ash	7.00	8.16
% Oxygen(diff)	11.85	13.82
	100.00	100.00

SULFUR FORMS

	As Rec'd	Dry
%Pyritic Sulfur	0.38	0.44
%Sulfate Sulfur	0.03	0.04
%Organic Sul. (dif)	0.64	0.74
Total Sulfur	1.05	1.22

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser
R. A. HOUSER, Manager, Midwest Division

RAH:lf



Charter Member

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 284-1173



Oct. 14, 1977

KVB, INC.
600 S. County Road 18
Minneapolis, MN 54426

Sample identification
by

KVB, Inc.

Kind of sample
reported to us -----

Site A Test 5

Sample taken at -----

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. 71-7342 PROXIMATE ANALYSIS

	<u>As received</u>	<u>Dry basis</u>
% Moisture	15.33	xxxxxx
% Ash	5.21	6.14
% Volatile	34.29	40.45
% Fixed Carbon	45.27	53.41
	<u>100.00</u>	<u>100.00</u>
Btu	10588	12489
% Sulfur	1.02	1.20

FUSION TEMPERATURE OF ASH

	<u>Reducing</u>	<u>Oxidizing</u>
Initial Deformation	XXXXXX	XXXXXX
Softening (H-W)	XXXXXX	XXXXXX
Softening (H-½W)	XXXXXX	XXXXXX
Fluid	XXXXXX	XXXXXX

H is Cone Height
W is Cone Width

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. HOUSER, Manager, Midwest Division



RAH:lf

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



Jan. 11, 1978

KVB INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 54226

Att: Peter L. Langsjoen

Sample identification
by

KVB Inc.

Kind of sample
reported to us -----

Coal Test 8

Sample taken at -----

Sample taken by KVB Inc.

Date sampled -----

Analysis report no. 71-11218
PROXIMATE ANALYSIS

	<u>As received</u>	<u>Dry basis</u>
% Moisture	13.10	XXXXX
% Ash	5.79	6.66
% Volatile	35.18	40.48
% Fixed Carbon	45.93	52.86
	<u>100.00</u>	<u>100.00</u>
Btu	10838	12471
% Sulfur	0.97	1.12

FUSION TEMPERATURE OF ASH

	<u>Reducing</u>	<u>Oxidizing</u>	
Initial Deformation	XXXXX	XXXXX	H is Cone Height
Softening (H-W)	XXXXX	XXXXX	W is Cone Width
Softening (H-1/2W)	XXXXX	XXXXX	
Fluid	XXXXX	XXXXX	

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. HOUSER, Manager, Midwest Division



RAH:lf

Charter Member

CHICAGO, ILLINOIS • CHARLESTON, W.VA. • CLARKSBURG, W.VA. • CLEVELAND, OHIO • NORFOLK, VA. • HENDERSON, KY. • TOLEDO, OHIO • DENVER, COLORADO • BIRMINGHAM, ALABAMA • VANCOUVER, B.C.

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 - AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



Jan. 11, 1978

KVB INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 55426
Att: Peter L. Langsjoen

Sample identification
by

KVB Inc.

Kind of sample
reported to us -----

Bottom Ash Test 8

Sample taken at -----

Sample taken by KVB Inc.

Date sampled -----

Analysis report no. 71-11215

%Sulfur, Dry ----- 0.05

RAH:lf

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser
R. A. HOUSER, Manager, Chicago Office



Charter Member
CHICAGO, ILLINOIS • CHARLESTON, W.VA. • CLARKSBURG, W.VA. • CLEVELAND, OHIO • NORFOLK, VA. • HENDERSON, KY • TOLEDO, OHIO • DENVER, COLORADO • BIRMINGHAM, ALABAMA • VANCOUVER, B.C.

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
18130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



Jan. 11, 1978

KVB INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 55426

Att: Peter L. Langsjoen

Sample identification
by

KVB Inc.

Kind of sample
reported to us -----

Coal Test 9

Sample taken at -----

Sample taken by KVB Inc.

Date sampled -----

Analysis report no. 71-11219 PROXIMATE ANALYSIS

	<u>As received</u>	<u>Dry basis</u>
% Moisture	14.57	xxxxx
% Ash	5.95	6.96
% Volatile	34.79	40.72
% Fixed Carbon	44.69	52.32
	<u>100.00</u>	<u>100.00</u>
Btu	10637	12451
% Sulfur	0.91	1.06

FUSION TEMPERATURE OF ASH

	<u>Reducing</u>	<u>Oxidizing</u>	
Initial Deformation	xxxxx	xxxxx	H is Cone Height
Softening (H-W)	xxxxx	xxxxx	W is Cone Width
Softening (H-1/2W)	xxxxx	xxxxx	
Fluid	xxxxx	xxxxx	

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. FROESCH, Manager, Midwest Division



RAH:lf

199

Charter Member

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PLEASE ADDRESS ALL CORRESPONDENCE TO:
18130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473



OFFICE TEL. (312) 284-1173

Jan. 11, 1978

KVB INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 54426

Att: Peter L. Langsjoen

Sample identification
by
KVB Inc.

Kind of sample
reported to us -----

Bottom Ash Test 9

Sample taken at -----

Sample taken by KVB Inc.

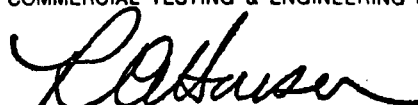
Date sampled -----

Analysis report no. 71-11216

%Sulfur, Dry ----- 0.06

RAH:lf

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.


R. A. HOUSER, Manager, Midwest Division

200



Charter Member

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



April 28, 1978

KVB, INC.
Shelard tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 54426

Kind of sample
reported to us -----

Sample taken at -----

Sample taken by KVB, Inc.

Date sampled -----

Sample Identification
by

KVB, Inc.

P. O. No. 323-15900

Coal Site A Test #10

Analysis report no. 71-13868

PROXIMATE ANALYSIS	As received	Dry basis	ULTIMATE ANALYSIS	As received	Dry basis
% Moisture	13.70	xxxxxx	Moisture	13.70	xxxxxx
% Ash	6.70	7.76	Carbon	60.30	69.87
% Volatile	34.33	39.78	Hydrogen	4.08	4.73
% Fixed Carbon	45.27	52.46	Nitrogen	0.96	1.11
	100.00	100.00	Chlorine	0.02	0.02
			Sulfur	0.92	1.07
Btu	10505	12173	Ash	6.70	7.76
% Sulfur	0.92	1.07	Oxygen (diff)	13.32	15.44
% Alk. as Na ₂ O	xxxxxx	0.08		100.00	100.00

SULFUR FORMS		
% Pyritic Sulfur	xxxxxx	xxxxxx
% Sulfate Sulfur	xxxxxx	xxxxxx
% Organic Sulfur	xxxxxx	xxxxxx

MINERAL ANALYSIS OF ASH	% Weight Ignited Basis
Silica; SiO ₂	59.32
Alumina, Al ₂ O ₃	12.90
Titania, TiO ₂	0.55
Ferric oxide, Fe ₂ O ₃	11.10
Lime, CaO	5.92
Magnesia, MgO	2.16
Potassium oxide, K ₂ O	1.06
Sodium oxide, Na ₂ O	0.32

WATER SOLUBLE ALKALIES

% Na ₂ O =	xxxxxx
% K ₂ O =	xxxxxx

FUSION TEMPERATURE OF ASH

	Reducing	Oxidizing
Initial Deformation	2000°F	2120 °F
Softening (H = W)	2190°F	2410 °F
Softening (H = ½ W)	2240°F	2470 °F
Fluid	2640°F	2700+°F

Sulfur trioxide, SO ₃	5.71
Phos. pentoxide, P ₂ O ₅	0.19
Undetermined	0.77
	100.00

% EQUILIBRIUM MOISTURE =	xxxxxx
HARDGROVE GRINDABILITY INDEX =	xxxxxx
FREE SWELLING INDEX =	xxxxxx

SILICA VALUE =	75.57
BASE: ACID RATIO	0.28
T ₂₅₀ Temperature =	2590°F

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser
R. A. HOUSER, Manager Midwest Division
201



RAH: lau

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 728-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
18130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 284-1173



April 26, 1978

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 55426

Sample identification
by

KVB, Inc.

Kind of sample
reported to us -----

Coal Stie A
Test #12

Sample taken at -----

P. O. No. 323-15900

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. 71-13869

PROXIMATE ANALYSIS

	<u>As received</u>	<u>Dry basis</u>
% Moisture	13.36	xxxxxx
% Ash	5.70	6.58
% Volatile	35.15	40.57
% Fixed Carbon	45.79	52.85
	<u>100.00</u>	<u>100.00</u>
Btu	10548	12174
% Sulfur	0.88	1.01

FUSION TEMPERATURE OF ASH

	<u>Reducing</u>	<u>Oxidizing</u>
Initial Deformation	xxxxxx	xxxxxx
Softening (H-W)	xxxxxx	xxxxxx
Softening (H-1/2W)	xxxxxx	xxxxxx
Fluid	xxxxxx	xxxxxx

H is Cone Height

W is Cone Width

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser
R. A. HOUSER, Manager, Midwest Division
202



RAH: lau

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



Oct. 14, 1977

KVB, INC.
600 S. County Road 18
Minneapolis, MN 54426

Sample identification-
by

KVB, Inc.

Kind of sample
reported to us -----

Site A Test 14

Sample taken at -----

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. 71-7343 PROXIMATE ANALYSIS

	<u>As received</u>	<u>Dry basis</u>
% Moisture	14.61	xxxxxx
% Ash	4.49	5.26
% Volatile	35.03	41.02
% Fixed Carbon	45.87	53.72
	<u>100.00</u>	<u>100.00</u>
Btu	10780	12624
% Sulfur	0.90	1.05

FUSION TEMPERATURE OF ASH

	<u>Reducing</u>	<u>Oxidizing</u>
Initial Deformation	xxxxxx	xxxxxx
Softening (H-W)	xxxxxx	xxxxxx
Softening (H-½W)	xxxxxx	xxxxxx
Fluid	xxxxxx	xxxxxx

H is Cone Height
W is Cone Width

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. HOUSER, Manager, Midwest Division

203



Charter Member

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601-- AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473



OFFICE TEL. (312) 264-1173

April 26, 1978

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 55426

Sample identification
by

KVB, Inc.

P. O. No. 323-15900

See Below for Identification

Kind of sample
reported to us -----

Sample taken at -----

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. See Below

LAB NUMBER

71-13882

IDENTIFICATION

Bottom Ash Site A Test #14

%ASH (DRY)

99.26

RAH: lau

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser, Manager, Midwest Division

204



Charter Member

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COMMERCIAL TESTING & ENGINEERING CO.

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PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 284-1173



April 26, 1978

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 54426

Sample identification
by
KVB, Inc.

Kind of sample
reported to us -----

Coal Site A
Test #15

Sample taken at -----

P. O. No. 323-15900

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. 71-13870 PROXIMATE ANALYSIS

	<u>As received</u>	<u>Dry basis</u>
% Moisture	13.56	xxxxx
% Ash	6.13	7.09
% Volatile	35.69	41.29
% Fixed Carbon	44.62	51.62
	<u>100.00</u>	<u>100.00</u>
Btu	10567	12225
% Sulfur	0.86	1.00

FUSION TEMPERATURE OF ASH

	<u>Reducing</u>	<u>Oxidizing</u>
Initial Deformation	xxxxx	xxxxx
Softening (H-W)	xxxxx	xxxxx
Softening (H-½W)	xxxxx	xxxxx
Fluid	xxxxx	xxxxx

H is Cone Height
W is Cone Width

RAH:1au

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser
R. A. HOUSER, Manager, Midwest Division
205



Charter Member

COMMERCIAL TESTING & ENGINEERING CO.

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PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



Oct. 14, 1977

KVB, INC.
600 S. County Road 18
Minneapolis, MN 54426

Sample identification
by

KVB, Inc.

Site A Test 16

Kind of sample
reported to us -----

Sample taken at -----

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. 71-7344 PROXIMATE ANALYSIS

	<u>As received</u>	<u>Dry basis</u>
% Moisture	17.85	xxxxxx
% Ash	6.79	8.26
% Volatile	33.20	40.42
% Fixed Carbon	42.16	51.32
	<u>100.00</u>	<u>100.00</u>
Btu	9969	12136
% Sulfur	0.62	0.76

FUSION TEMPERATURE OF ASH

	<u>Reducing</u>	<u>Oxidizing</u>
Initial Deformation	XXXXX	XXXXX
Softening (H-W)	XXXXX	XXXXX
Softening (H-½W)	XXXXX	XXXXX
Fluid	XXXXX	XXXXX

H is Cone Height
W is Cone Width

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. HOUSER, Manager, Midwest Division

RAH:lf

206



COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601~ AREA CODE 312 728-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
18130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473



OFFICE TEL. (312) 284-1173

April 26, 1978

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 54426

Sample Identification
by

Kind of sample
reported to us -----

KVB, Inc.

P. O. No. 323-15900

Sample taken at -----

See Below for Identification

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. See Below

LAB NUMBER

71-13883

IDENTIFICATION

Bottom Ash Site A Test #16

ASH (DRY)

99.88

RAH:1au

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser
R. A. Houser, Manager, Midwest Division

207



Charter Member

CHICAGO, IL • BILLINGS, MT • BIRMINGHAM, AL • CHARLESTON, WV • CLARKSBURG, WV • CLEVELAND, OH • DENVER, CO • GOLDEN, CO • HENDERSON, KY •
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COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 728-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



April 26, 1978

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 55426

Sample identification
by

KVB, Inc.

Kind of sample
reported to us -----

Coal Site A
Test #17

Sample taken at -----

P. O. No. 323-15900

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. 71-13871 PROXIMATE ANALYSIS

	<u>As received</u>	<u>Dry basis</u>
% Moisture	17.80	xxxxx
% Ash	3.94	4.79
% Volatile	35.72	43.45
% Fixed Carbon	42.54	51.76
	100.00	100.00
Btu	10350	12591
% Sulfur	0.63	0.77

FUSION TEMPERATURE OF ASH

	<u>Reducing</u>	<u>Oxidizing</u>
Initial Deformation	xxxxx	xxxxx
Softening (H-W)	xxxxx	xxxxx
Softening (H-½W)	xxxxx	xxxxx
Fluid	xxxxx	xxxxx

H is Cone Height
W is Cone Width

RAH: lau

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.


R. A. HOUSER, Manager, Midwest Division
208



Charter Member

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 - AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473



April 26, 1978

OFFICE TEL. (312) 264-1173

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 54426

Sample identification
by

KVB, Inc.

P. O. No. 323-15900

See Below for Identification

Kind of sample
reported to us -----

Sample taken at -----

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. See Below

LAB NUMBER

71-13884

IDENTIFICATION

Bottom Ash Site A Test #17

%ASH (DRY)

99.72

RAH: lau

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

A. A. Houser
A. A. Houser, Manager, Midwest Division



Charter Member

209

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COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 238 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 728-8434

OFFICE TEL. (312) 284-1173

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473



Jan. 11, 1978

KVB INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 55426

Att: Peter L. Langsjoen

Sample identification
by

KVB, Inc.

Kind of sample
reported to us -----

Coal Test 18

Sample taken at -----

Sample taken by KVB Inc.

Date sampled -----

Analysis report no. 71-11220
PROXIMATE ANALYSIS

	<u>As received</u>	<u>Dry basis</u>
% Moisture	15.05	xxxxxx
% Ash	5.90	6.94
% Volatile	34.72	40.87
% Fixed Carbon	44.33	52.19
	<u>100.00</u>	<u>100.00</u>
Btu	10538	12405
% Sulfur	0.88	1.04

FUSION TEMPERATURE OF ASH

	<u>Reducing</u>	<u>Oxidizing</u>
Initial Deformation	XXXXXX	XXXXXX
Softening (H-W)	XXXXXX	XXXXXX
Softening (H-½W)	XXXXXX	XXXXXX
Fluid	XXXXXX	XXXXXX

H is Cone Height
W is Cone Width

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser
R. A. HOUSER, Manager, Midwest Division

RAH:lf



210

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 728-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473



OFFICE TEL. (312) 264-1173

Jan. 11, 1978

KVB INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 54426

Att: Peter L. Langsjoen

Sample identification
by

KVB Inc.

Kind of sample
reported to us -----

Bottom Ash Test 18

Sample taken at -----

Sample taken by KVB Inc.

Date sampled -----

Analysis report no. 71-11217

%Sulfur, Dry ----- 0.16

RAH:lf

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.


R. A. HOUSER, Manager, Midwest Division



Charter Member

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 284-1173



Oct. 14, 1977

KVB, INC.
600 S. County Road 18
Minneapolis, MN 55426

Sample identification
by

KVB, Inc.

Kind of sample
reported to us -----

Site A Test 19

Sample taken at -----

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. 71-7345 PROXIMATE ANALYSIS

	<u>As received</u>	<u>Dry basis</u>
% Moisture	15.64	xxxxxx
% Ash	8.04	9.53
% Volatile	33.97	40.27
% Fixed Carbon	42.35	50.20
	<u>100.00</u>	<u>100.00</u>
Btu	10107	11980
% Sulfur	0.92	1.09

FUSION TEMPERATURE OF ASH

	<u>Reducing</u>	<u>Oxidizing</u>
Initial Deformation	xxxxxx	xxxxxx
Softening (H=W)	xxxxxx	xxxxxx
Softening (H=½W)	xxxxxx	xxxxxx
Fluid	xxxxxx	xxxxxx

H is Cone Height
W is Cone Width

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

RAH:lf

R. A. HOUSER, Manager, Midwest Division

212



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PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



April 26, 1978

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 54426

Sample identification
by
KVB, Inc.

Kind of sample
reported to us -----

Coal Site A
Test #21

Sample taken at -----

P. O. No. 323-15900

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. 71-13872 PROXIMATE ANALYSIS

	<u>As received</u>	<u>Dry basis</u>
% Moisture	17.83	xxxxxx
% Ash	2.65	3.23
% Volatile	35.99	43.80
% Fixed Carbon	43.53	52.97
	<u>100.00</u>	<u>100.00</u>
Btu	10514	12795
% Sulfur	0.49	0.60

FUSION TEMPERATURE OF ASH

	<u>Reducing</u>	<u>Oxidizing</u>	
Initial Deformation	xxxxxx	xxxxxx	H is Cone Height
Softening (H-W)	xxxxxx	xxxxxx	W is Cone Width
Softening (H-½W)	xxxxxx	xxxxxx	
Fluid	xxxxxx	xxxxxx	

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. HOUSER, Manager, Midwest Division

RAH:1au



213

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473



April 26, 1978

OFFICE TEL. (312) 264-1173

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 54426

Sample Identification
by

KVB, Inc.

Kind of sample
reported to us -----

P. O. No. 323-15900

Sample taken at -----

See Below for Identification

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. See Below

LAB NUMBER

71-13889

IDENTIFICATION

Multitone Ash Site A Test #21

%ASH (DRY)

23.30

RAH:1au

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser, Manager, Midwest Division



Charter Member

214

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COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



April 26, 1978

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 54426

Sample identification
by
KVB, Inc.

Kind of sample
reported to us -----

Coal Site A
Test #22

Sample taken at -----

P. O. No. 323-15900

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. 71-13873

PROXIMATE ANALYSIS

	<u>As received</u>	<u>Dry basis</u>
% Moisture	18.94	xxxxx
% Ash	2.63	3.25
% Volatile	34.45	42.50
% Fixed Carbon	43.98	54.25
	<u>100.00</u>	<u>100.00</u>
Btu	10338	12754
% Sulfur	0.54	0.67

FUSION TEMPERATURE OF ASH

	<u>Reducing</u>	<u>Oxidizing</u>	
Initial Deformation	XXXXX	XXXXX	H is Cone Height
Softening (H-W)	XXXXX	XXXXX	W is Cone Width
Softening (H-½W)	XXXXX	XXXXX	
Fluid	XXXXX	XXXXX	

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser
R. A. HOUSER, Manager, Midwest Division



RAH: lau

215

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 728-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



Nov. 8, 1977

KVB, INC.
600 S. County Road 18
Minneapolis, MN 54426

Kind of sample
reported to us -----

Sample Identification
by

KVB, Inc.

Sample taken at -----

Site A Test 23

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. 71-7346

PROXIMATE ANALYSIS	As received	Dry basis	ULTIMATE ANALYSIS	As received	Dry basis
% Moisture	20.43	xxxxx	Moisture	20.43	xxxxx
% Ash	2.86	3.59	Carbon	58.97	74.11
% Volatile	34.61	43.50	Hydrogen	4.02	5.05
% Fixed Carbon	42.10	52.91	Nitrogen	0.72	0.91
	100.00	100.00	Chlorine	0.00	0.00
			Sulfur	0.56	0.70
Btu	10242	12871	Ash	2.86	3.59
% Sulfur	0.56	0.70	Oxygen (diff)	12.44	15.64
% Alk. as Na ₂ O	xxxxx	0.02		100.00	100.00

SULFUR FORMS

% Pyritic Sulfur	xxxxxx	xxxxxx
% Sulfate Sulfur	xxxxxx	xxxxxx
% Organic Sulfur	xxxxxx	xxxxxx

MINERAL ANALYSIS OF ASH

	% Weight Ignited Basis
Silica; SiO ₂	44.81
Alumina, Al ₂ O ₃	18.14
Titania, TiO ₂	0.62
Ferric oxide, Fe ₂ O ₃	4.04
Lime, CaO	11.65
Magnesia, MgO	3.92
Potassium oxide, K ₂ O	0.55
Sodium oxide, Na ₂ O	0.30

WATER SOLUBLE ALKALIES

% Na ₂ O =	xxxxxx	xxxxxx
% K ₂ O =	xxxxxx	xxxxxx

FUSION TEMPERATURE OF ASH

	Reducing	Oxidizing
Initial Deformation	xxxxxx	xxxxxx
Softening (H = W)	xxxxxx	xxxxxx
Softening (H = 1/2 W)	xxxxxx	xxxxxx
Fluid	xxxxxx	xxxxxx

% EQUILIBRIUM MOISTURE = xxxxxx
HARDGROVE GRINDABILITY INDEX = xxxxxx
FREE SWELLING INDEX = xxxxxx

Sulfur trioxide, SO ₃	14.93
Phos. pentoxide, P ₂ O ₅	0.12
Undetermined	0.92
	100.00

SILICA VALUE = 69.56
BASE: ACID RATIO 0.32
T₂₅₀ Temperature = 2515°F

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser

R. A. HOUSER, Manager Midwest Division

RAH:lf



Charter Member
ASTM

216

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 - AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 284-1173



Jan. 11, 1978

KVB INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 54426

Att: Peter L. Langsjoen

Sample identification
by

Kind of sample
reported to us -----

KVB Inc.

Bottom Ash Test 23

Sample taken at -----

Sample taken by KVB Inc.

Date sampled -----

Analysis report no. 71-11210

%Ash, Dry ----- 99.74

%Combustible, Dry ----- 0.26

RAH:lf

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. HOUSER, Manager, Midwest Division

217



Charter Member

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



Dec. 1, 1977

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, Minn. 54426

Sample identification
by

KVB, Inc.

Kind of sample
reported to us -----

Texas Gulf

Sample taken at -----

Coal Sample

Test 24

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. 71-10030

PROXIMATE ANALYSIS

	<u>As received</u>	<u>Dry basis</u>
% Moisture	19.56	xxxxxx
% Ash	2.92	3.63
% Volatile	34.67	43.10
% Fixed Carbon	42.85	53.27
	<u>100.00</u>	<u>100.00</u>
Btu	10323	12832
% Sulfur	0.58	0.72

FUSION TEMPERATURE OF ASH

	<u>Reducing</u>	<u>Oxidizing</u>
Initial Deformation	2260°F	2330°F
Softening (H-W)	2360°F	2400°F
Softening (H-½W)	2460°F	2485°F
Fluid	2565°F	2580°F

H is Cone Height
W is Cone Width

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. HOUSER, Manager, Midwest Division

RAH:lf



218

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 - AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
18130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



Jan. 11, 1978

KVB INC,
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 55426

Att: Peter L. Langsjoen

Sample identification
by

KVB Inc.

Kind of sample
reported to us -----

Bottom Ash Test 24

Sample taken at -----

Sample taken by KVB Inc.

Date sampled -----

Analysis report no. 71-11211

%Ash, Dry ----- 99.47

%Combustible, Dry ----- 0.53

RAH:lf

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser
R. A. HOUSER, Manager, Midwest Division



Charter Member

219

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 928 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
18130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 284-1173



Jan. 11, 1978

KVB INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 55426

Att: Peter L. Langsjoen

Sample identification
by

KVB Inc.

Kind of sample
reported to us -----

Multiclone Ash Test 24

Sample taken at -----

Sample taken by KVB Inc.

Date sampled -----

Analysis report no. 71-11223

SCREEN ANALYSIS		%ASH (DRY)	%COMBUSTIBLE (DRY)
Size	%Wt.		
+20M	4.3	27.44	72.56
20M X 100M	34.4	38.68	61.32
100M X 0	61.3	95.00	5.00
	100.0	Wtd. Average 72.72	27.28

RAH:lf

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser
R. A. HOUSER, Manager, Midwest Division



Charter Member

220

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 328 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 - AREA CODE 312 726-2424

PLEASE ADDRESS ALL CORRESPONDENCE TO:
6130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



April 26, 1978

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 55426

Sample identification
by

KVB, Inc.

Kind of sample
reported to us -----

Coal Site A

Test #26A

Sample taken at -----

P. O. No. 323-15900

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. 71-13874 PROXIMATE ANALYSIS

	<u>As received</u>	<u>Dry basis</u>
% Moisture	18.09	xxxxx
% Ash	3.27	3.99
% Volatile	35.31	43.11
% Fixed Carbon	43.33	52.90
	<u>100.00</u>	<u>100.00</u>
Btu	10487	12803
% Sulfur	0.75	0.91

FUSION TEMPERATURE OF ASH

	<u>Reducing</u>	<u>Oxidizing</u>
Initial Deformation	xxxxx	xxxxx
Softening (H-W)	xxxxx	xxxxx
Softening (H-½W)	xxxxx	xxxxx
Fluid	xxxxx	xxxxx

H is Cone Height
W is Cone Width

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser
R. A. HOUSER, Manager, Midwest Division

221



Charter Member

RAH: lau

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601- AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473



OFFICE TEL. (312) 264-1173

April 26, 1978

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 54426

Sample identification
by

KVB, Inc.

P. O. No. 323-15900

See Below for Identification

Kind of sample
reported to us -----

Sample taken at -----

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. See Below

LAB NUMBER

71-13885

IDENTIFICATION

Bottom Ash Site A Test #26A

ASH (DRY)

98.13

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser
R. A. Houser, Manager, Midwest Division



Charter Member

222

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RAH:1au

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473



OFFICE TEL. (312) 264-1173

► KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 55426

April 28, 1978

Sample identification
by
P. J. Langsjoen

Kind of sample reported to us Multiclone ash samples
Site A

Sample taken at xxxxxx

P. O. No. 323-15900

Sample taken by KVB, Inc.

Date sampled 4/11/78

Analysis report no. See below

<u>Analysis report No.</u>	<u>Identification</u>	<u>% Ash, Dry Basis</u>
71-13890	Test #26A	41.19
71-13891	Test #26B	25.83
71-13892	Test #28	19.41
71-13893	Test #29	41.27
71-13894	Test #36	31.55
71-13895	Test #38	45.29
71-13896	Test #39	51.94

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.


R. A. Houser, Manager, Midwest Division

RAH/dh



Charter Member

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COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:

16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



April 26, 1978

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 54426

Sample identification
by

KVB, Inc.

Kind of sample
reported to us -----

Coal Site A
Test #26B

Sample taken at -----

P. O. No. 323-15900

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. 71-13875 PROXIMATE ANALYSIS

	<u>As received</u>	<u>Dry basis</u>
% Moisture	20.42	xxxxxx
% Ash	3.14	3.95
% Volatile	33.92	42.62
% Fixed Carbon	42.52	53.43
	<u>100.00</u>	<u>100.00</u>
Btu	10158	12765
% Sulfur	0.77	0.97

FUSION TEMPERATURE OF ASH

	<u>Reducing</u>	<u>Oxidizing</u>
Initial Deformation	xxxxxx	xxxxxx
Softening (H-W)	xxxxxx	xxxxxx
Softening (H-½W)	xxxxxx	xxxxxx
Fluid	xxxxxx	xxxxxx

H is Cone Height
W is Cone Width

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Eglouser
R. A. EGLUSER, Manager, Midwest Division



RAH:lau

224

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473



OFFICE TEL. (312) 264-1173

April 26, 1978

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 54426

Sample identification
by

KVB, Inc.

P. O. No. 323-15900

See Below for Identification

Kind of sample
reported to us -----

Sample taken at -----

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. See Below

LAB NUMBER

71-13886

IDENTIFICATION

Bottom Ash Site A Test #26B

%ASH (DRY)

99.83

RAH: lau

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser
R. A. Houser, Manager, Midwest Division

225



Charter Member

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MIDDLESBORO, KY • MOBILE, AL • NEW ORLEANS, LA • NORFOLK, VA • PIKEVILLE, KY • VANCOUVER, B.C. CAN.

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473



OFFICE TEL. (312) 264-1173

June 2, 1978

KVB, INC.
Shelard Tower, Ste. 1357
600 S. County Road 18
Minneapolis, MN 55426

Sample identification
by

KVB, Inc.

Kind of sample
reported to us Coal

P. O. No. 323-15900

Sample taken at xxxxxx

Coal Sample
Boiler A
Test 27

Sample taken by KVB, Inc.

Date sampled xxxxxx

Analysis report no. 71-15019

PROXIMATE ANALYSIS

	As Rec'd	Dry Basis
%Moisture	17.17	xxxxxx
%Ash	3.54	4.27
%Volatile	35.04	42.30
%Fixed Carbon	44.25	53.43
	100.00	100.00
Btu	10393	12547
%Sulfur	0.85	1.03

ULTIMATE ANALYSIS

	As Rec'd	Dry Basis
%Moisture	17.17	xxxxxx
%Carbon	60.44	72.97
%Hydrogen	4.12	4.98
%Nitrogen	1.01	1.22
%Chlorine	0.01	0.01
%Sulfur	0.85	1.03
%Ash	3.54	4.27
%Oxygen (diff)	12.86	15.52
	100.00	100.00

MINERAL ANALYSIS

	%Weight, Ign.
Silica, SiO ₂	41.66
Alumina, Al ₂ O ₃	18.29
Titania, TiO ₂	0.66
Ferric Oxide, Fe ₂ O ₃	4.49
Lime, CaO	12.25
Magnesia, MgO	4.20
Potassium Oxide, K ₂ O	0.50
Sodium Oxide, Na ₂ O	0.32
Sulfur Trioxide, SO ₃	17.15
Phos. Pent. P ₂ O ₅	0.15
Undetermined	0.33
	100.00
Alk. as Na ₂ O, Dry Coal =	0.03
SILICA VALUE =	66.55
Base/Acid =	0.36
T250 Poises:	2460°F

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser
R. A. Houser, Manager, Midwest Division



Charter Member

RAH:lau

226

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MIDDLESBORO, KY • MOBILE, AL • NEW ORLEANS, LA • NORFOLK, VA • PIKEVILLE, KY • VANCOUVER, B.C. CAN.

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 - AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:

16136 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



April 26, 1978

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 54426

Sample identification

by

KVB, Inc.

Kind of sample
reported to us -----

Coal Site A
Test #28

P. O. No. 323-15900

Sample taken at -----

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. 71-13876

PROXIMATE ANALYSIS

	<u>As received</u>	<u>Dry basis</u>
% Moisture	18.29	xxxxx
% Ash	3.02	3.69
% Volatile	34.78	42.57
% Fixed Carbon	43.91	53.74
	<u>100.00</u>	<u>100.00</u>
Btu	10475	12819
% Sulfur	0.65	0.80

FUSION TEMPERATURE OF ASH

	<u>Reducing</u>	<u>Oxidizing</u>
Initial Deformation	XXXXX	XXXXX
Softening (H-W)	XXXXX	XXXXX
Softening (H-½W)	XXXXX	XXXXX
Fluid	XXXXX	XXXXX

H is Cone Height

W is Cone Width

RAH: lau

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. HOUSER, Manager, Midwest Division

227



Charter Member

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



Dec. 1, 1977

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, Minn. 54426

Sample identification
by

KVB, Inc.

Kind of sample
reported to us -----

Coal Sample

Test Side A

Sample taken at -----

Test 29

Sample taken by KVB, Inc.

Date sampled -----

ULTIMATE ANALYSIS

Analysis report no. 71-10031

PROXIMATE ANALYSIS

	<u>As received</u>	<u>Dry basis</u>
% Moisture	19.79	xxxxxx
% Ash	2.80	3.49
% Volatile	34.75	43.32
% Fixed Carbon	42.66	53.19
	100.00	100.00
Btu	10372	12930
% Sulfur	0.59	0.73

	<u>As Rec'd</u>	<u>Dry</u>
%Moisture	19.79	xxxxxx
%Carbon	60.30	75.18
%Hydrogen	4.09	5.10
%Nitrogen	0.83	1.03
%Chlorine	0.02	0.02
%Sulfur	0.59	0.73
%Ash	2.80	3.49
%Oxygen(dif)	11.58	14.45
	100.00	100.00

FUSION TEMPERATURE OF ASH

	<u>Reducing</u>	<u>Oxidizing</u>
Initial Deformation	2180°F	2285°F
Softening (H-W)	2240°F	2385°F
Softening (H-½W)	2325°F	2485°F
Fluid	2410°F	2600°F

H is Cone Height
W is Cone Width

RAH:lf

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. HOUSER, Manager, Midwest Division



228

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:

16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



Jan. 11, 1978

KVB INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 55426

Att: Peter L. Langsjoen

Sample identification
by
KVB Inc.

Kind of sample
reported to us -----

Bottom Ash Test 29

Sample taken at -----

Sample taken by KVB Inc.

Date sampled -----

Analysis report no. 71-11212

%Ash, Dry ----- 100.06

%Combustible, Dry ----- *

*Ash = over 100%

RAH:lf

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.


R. A. HOUSER, Manager, Midwest Division

229



Charter Member

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COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 728-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



April 26, 1978

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 55426

Sample identification
by

Kind of sample
reported to us -----

KVB, Inc.

Coal Site A
Test #30

Sample taken at -----

P. O. No. 323-15900

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. 71-13877 PROXIMATE ANALYSIS

	<u>As received</u>	<u>Dry basis</u>
% Moisture	20.34	XXXXXX
% Ash	2.81	3.53
% Volatile	34.63	43.47
% Fixed Carbon	42.22	53.00
	<u>100.00</u>	<u>100.00</u>
Btu	10202	12807
% Sulfur	0.53	0.67

FUSION TEMPERATURE OF ASH

	<u>Reducing</u>	<u>Oxidizing</u>
Initial Deformation	XXXXXX	XXXXXX
Softening (H-W)	XXXXXX	XXXXXX
Softening (H-½W)	XXXXXX	XXXXXX
Fluid	XXXXXX	XXXXXX

H is Cone Height
W is Cone Width

RAH:lau

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. HOUSE, Manager, Midwest Division



230

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 728-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
18130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 284-1173



Dec. 1, 1977

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, Minn. 54426

Sample identification
by

KVB, Inc.

Kind of sample
reported to us -----

Boiler A

Coal Sample

Sample taken at -----

Test 34

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. 71-10032 PROXIMATE ANALYSIS

	<u>As received</u>	<u>Dry basis</u>
% Moisture	12.72	xxxxxx
% Ash	8.79	10.07
% Volatile	33.82	38.75
% Fixed Carbon	44.67	51.18
	<u>100.00</u>	<u>100.00</u>
Btu	10534	12069
% Sulfur	0.73	0.42

FUSION TEMPERATURE OF ASH

	<u>Reducing</u>	<u>Oxidizing</u>	
Initial Deformation	xxxxxx	xxxxxx	H is Cone Height
Softening (H-W)	xxxxxx	xxxxxx	W is Cone Width
Softening (H-½W)	xxxxxx	xxxxxx	
Fluid	xxxxxx	xxxxxx	

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser
R. A. HOUSER, Manager, Midwest Division

RAH:lf



231

Charter Member

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COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 · AREA CODE 312 728-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
18130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



Jan. 11, 1978

KVB INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 55426

Att: Peter L. Langsjoen

Sample identification
by
KVB Inc.

Kind of sample
reported to us -----

Bottom Ash Test 34

Sample taken at -----

Sample taken by KVB Inc.

Date sampled -----

Analysis report no. 71-11213

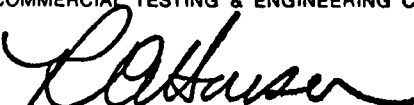
%Ash, Dry ----- 99.18

%Combustible, Dry --- 0.82

%Sulfur, Dry ----- 0.01

RAH;f

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.


R. A. HOUSER, Manager, Midwest Division

232



Charter Member

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



Jan. 11, 1978

KVB INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 54426

Att: Peter L. Langsjoen

Sample identification
by

KVB Inc.

Kind of sample
reported to us -----

Multiclone Ash Test 34

Sample taken at -----

Sample taken by KVB Inc.

Date sampled -----

Analysis report no. 71-11221

%Ash, Dry ----- 33.36

%Combustible, Dry--- 66.64

%Sulfur, Dry----- 0.37

RAH:1f

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.


R. A. HOUSER, Manager, Midwest Division

233



Charter Member

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 284-1173



Dec. 9, 1977

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, Minn. 54426

Kind of sample
reported to us -----

Sample taken at -----

Sample taken by KVB, Inc.

Date sampled -----

Sample Identification
by KVB, Inc.

Boiler A

Coal Sample

Test 35

Analysis report no. 71-10033

PROXIMATE ANALYSIS	Analysis report no. 71-10033		ULTIMATE ANALYSIS	% Weight	
	As received	Dry basis		As received	Dry basis
% Moisture	13.06	xxxxxx	Moisture	13.06	xxxxxx
% Ash	7.81	8.98	Carbon	62.19	71.54
% Volatile	34.37	39.54	Hydrogen	4.11	4.73
% Fixed Carbon	44.76	51.48	Nitrogen	0.82	0.94
	100.00	100.00	Chlorine	0.01	0.01
			Sulfur	0.35	0.40
Btu	10683	12288	Ash	7.81	8.98
% Sulfur	0.35	0.40	Oxygen (diff)	11.65	13.40
% Alk. as Na ₂ O	xxxxxx	0.13		100.00	100.00

SULFUR FORMS		
% Pyritic Sulfur	xxxxxx	xxxxxx
% Sulfate Sulfur	xxxxxx	xxxxxx
% Organic Sulfur	xxxxxx	xxxxxx

WATER SOLUBLE ALKALIES

% Na ₂ O =	xxxxxx	xxxxxx
% K ₂ O =	xxxxxx	xxxxxx

FUSION TEMPERATURE OF ASH

	Reducing	Oxidizing
Initial Deformation	2170°F	2300°F
Softening (H = W)	2265°F	2405°F
Softening (H = 1/2 W)	2355°F	2510°F
Fluid	2420°F	2610°F

% EQUILIBRIUM MOISTURE = xxxxxx
HARDGROVE GRINDABILITY INDEX = xxxxxx
FREE SWELLING INDEX = xxxxxx

MINERAL ANALYSIS OF ASH

MINERAL ANALYSIS OF ASH		% Weight Ignited Basis
Silica, SiO ₂		46.02
Alumina, Al ₂ O ₃		18.65
Titania, TiO ₂		0.70
Ferric oxide, Fe ₂ O ₃		6.96
Lime, CaO		14.80
Magnesia, MgO		1.62
Potassium oxide, K ₂ O		0.65
Sodium oxide, Na ₂ O		1.02
Sulfur trioxide, SO ₃		8.23
Phos. pentoxide, P ₂ O ₅		0.78
Undetermined		0.57
		100.00

SILICA VALUE = 66.31
BASE: ACID RATIO 0.38
T₂₅₀ Temperature = 2435°F

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser

R. A. HOUSER, Manager Midwest Division



Charter Member

234

RAH:lf

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 728-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:

16138 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 284-1173



Jan. 11, 1978

KVB INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 55426
Att: Peter L. Langsjoen

Sample identification
by
KVB Inc.

Kind of sample
reported to us -----

Bottom Ash Test 35

Sample taken at -----

Sample taken by KVB Inc.

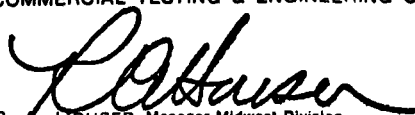
Date sampled -----

Analysis report no. 71-11214

%Ash, Dry ----- 98.34
%Combustible, Dry --- 1.66
%Sulfur, Dry ----- 0.02

RAH:lf

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.


R. A. HOUSER, Manager, Midwest Division

235



Charter Member

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 - AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



Jan. 11, 1978

KVB INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 54426
Att: Peter L. Langsjoen

Sample identification
by

KVB Inc.

Kind of sample
reported to us -----

Multiclone Ash Test 35

Sample taken at -----

Sample taken by KVB Inc.

Date sampled -----

Analysis report no. 71-11222

%Ash, Dry ----- 29.98

%Combustible, Dry ---- 70.02

%Sulfur, Dry ----- 0.32

RAH:lf

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser
R. A. HOUSER, Manager, Midwest Division

236



Charter Member

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16139 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



April 26, 1978

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 54426

Sample identification
by

KVB, Inc.

Kind of sample
reported to us -----

Coal Site A
Test #36

Sample taken at -----

P. O. No. 323-15900

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. 71-13878

PROXIMATE ANALYSIS

	As received	Dry basis
	12.72	xxxxxx
% Moisture	6.14	7.04
% Ash	34.60	39.64
% Volatile	46.54	53.32
% Fixed Carbon	100.00	100.00
	10920	12511
Btu	0.31	0.36
% Sulfur		

FUSION TEMPERATURE OF ASH

	Reducing	Oxidizing
Initial Deformation	XXXXX	XXXXX
Softening (H-W)	XXXXX	XXXXX
Softening (H-½W)	XXXXX	XXXXX
Fluid	XXXXX	XXXXX

H is Cone Height
W is Cone Width

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. HOUSER, Manager, Midwest Division



RAH:lau

237

Charter Member

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 728-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 284-1173



April 26, 1978

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 54426

Sample identification
by

KVB, Inc.

Kind of sample
reported to us -----

Coal Site A
Test #37

Sample taken at -----

P. O. No. 323-15900

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. 71-13879 PROXIMATE ANALYSIS

	<u>As received</u>	<u>Dry basis</u>
% Moisture	11.29	xxxxx
% Ash	8.23	9.28
% Volatile	34.34	38.71
% Fixed Carbon	46.14	52.01
	<u>100.00</u>	<u>100.00</u>
Btu	10768	12138
% Sulfur	0.28	0.32

FUSION TEMPERATURE OF ASH

	<u>Reducing</u>	<u>Oxidizing</u>
Initial Deformation	XXXXX	XXXXX
Softening (H-W)	XXXXX	XXXXX
Softening (H-½W)	XXXXX	XXXXX
Fluid	XXXXX	XXXXX

H is Cone Height
W is Cone Width

RAH:lau

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser
R. A. HOUSER, Manager, Midwest Division



238

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 728-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
18130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 284-1173



April 26, 1978

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 55426

Sample identification
by

KVB, Inc.

Kind of sample
reported to us -----

Coal Site A
Test #38

Sample taken at -----

P. O. No. 323-15900

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. 71-13880 PROXIMATE ANALYSIS

	<u>As received</u>	<u>Dry basis</u>
% Moisture	12.87	xxxxxx
% Ash	8.71	10.00
% Volatile	33.96	38.98
% Fixed Carbon	44.46	51.02
	<u>100.00</u>	<u>100.00</u>
Btu	10479	12026
% Sulfur	0.32	0.37

FUSION TEMPERATURE OF ASH

	<u>Reducing</u>	<u>Oxidizing</u>	
Initial Deformation	xxxxxx	xxxxxx	H is Cone Height
Softening (H-W)	xxxxxx	xxxxxx	W is Cone Width
Softening (H-1/2W)	xxxxxx	xxxxxx	
Fluid	xxxxxx	xxxxxx	

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser
R. A. HOUSER, Manager, Midwest Division



239

Charter Member

RAH: lau

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473



April 26, 1978

OFFICE TEL. (312) 264-1173

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 54426

Sample identification
by

KVB, Inc.

Kind of sample
reported to us -----

P. O. No. 323-15900

Sample taken at -----

See Below for Identification

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. See Below

LAB NUMBER

71-13887

IDENTIFICATION

Bottom Ash Site A Test #38

%ASH (DRY)

99.77

RAH: lau

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser
R. A. Houser, Manager, Midwest Division

240



Charter Member

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MIDDLESBORO, KY • MOBILE, AL • NEW ORLEANS, LA • NORFOLK, VA • PIKEVILLE, KY • VANCOUVER, B.C. CAN.

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
5130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473

OFFICE TEL. (312) 264-1173



April 26, 1978

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 55426

Sample identification
by

KVB, Inc.

Kind of sample
reported to us -----

Coal Site A
Test #39

Sample taken at -----

P. O. No. 323-15900

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. 71-13881 PROXIMATE ANALYSIS

	<u>As received</u>	<u>Dry basis</u>
% Moisture	14.28	xxxxxx
% Ash	7.68	8.96
% Volatile	33.79	39.42
% Fixed Carbon	44.25	51.62
	<u>100.00</u>	<u>100.00</u>
Btu	10386	12116
% Sulfur	0.40	0.47

FUSION TEMPERATURE OF ASH

	<u>Reducing</u>	<u>Oxidizing</u>	
Initial Deformation	XXXXXX	XXXXXX	H is Cone Height
Softening (H-W)	XXXXXX	XXXXXX	W is Cone Width
Softening (H-1/2W)	XXXXXX	XXXXXX	
Fluid	XXXXXX	XXXXXX	

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. HOUSER, Manager, Midwest Division

241



Charter Member

RAH: lau

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
16130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473



OFFICE TEL. (312) 264-1173

April 26, 1978

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 55426

Sample identification
by

Kind of sample
reported to us -----

KVB, Inc.

P. O. No. 323-15900

Sample taken at -----

See Below for Identification

Sample taken by KVB, Inc.

Date sampled -----

Analysis report no. See Below

LAB NUMBER

71-13888

IDENTIFICATION

Bottom Ash Site A Test #39

ASH (DRY)

97.20

RAH:lau

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser, Manager, Midwest Division



Charter Member

242

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MIDDLESBORO, KY • MOBILE, AL • NEW ORLEANS, LA • NORFOLK, VA • PIKEVILLE, KY • VANCOUVER, B.C. CAN.

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 228 NORTH LA SALLE STREET, CHICAGO, ILLINOIS 60601 • AREA CODE 312 726-8434

PLEASE ADDRESS ALL CORRESPONDENCE TO:
18130 VAN DRUNEN ROAD, SOUTH HOLLAND, ILLINOIS 60473



OFFICE TEL. (312) 264-1173

May 26, 1978

KVB, INC.
Shelard Tower, Ste. 1375
600 S. County Road 18
Minneapolis, MN 55426

Sample Identification
by

Kind of sample
reported to us Coal

KVB, Inc.

Coal Sample
Boiler A
Test 40

Sample taken at xxxxxx

Sample taken by KVB, Inc.

Date sampled xxxxxx

Analysis report no. - 71-15020

PROXIMATE ANALYSIS

	As Rec'd	Dry Basis
%Moisture	17.83	xxxxx
%Ash	4.58	5.57
%Volatile	34.05	41.44
%Fixed Carbon	43.54	52.99
	100.00	100.00
Btu	10206	12420
%Sulfur	0.63	0.77

MINERAL ANALYSIS

	%Weight, Ign.
Silica, SiO ₂	51.88
Alumina, Al ₂ O ₃	18.49
Titania, TiO ₂	0.75
Ferric Oxide, Fe ₂ O ₃	5.02
Lime, CaO	8.12
Magnesia, MgO	2.76
Potassium Oxide, K ₂ O	0.90
Sodium Oxide, Na ₂ O	0.32

ULTIMATE ANALYSIS

	As Rec'd	Dry Basis
%Moisture	17.83	xxxxx
%Carbon	58.99	71.79
%Hydrogen	4.08	4.97
%Nitrogen	0.84	1.02
%Chlorine	0.00	0.00
%Sulfur	0.63	0.77
%Ash	4.58	5.57
%Oxygen (diff)	13.05	15.88
	100.00	100.00

Sulfur Trioxide, SO ₃	10.77
Phos. Pent. P ₂ O ₅	0.18
Undetermined	0.81
	100.00

Alk. As Na₂O, Dry Coal: 0.05

SILICA VALUE: 76.54

Base/Acid: 0.24

T250 Poises: 2665°F

Respectfully submitted,
COMMERCIAL TESTING & ENGINEERING CO.

R. A. Houser

R. A. Houser, Manager, Midwest Division



Charter Member

RAH:1au

243

CHICAGO, IL • BILLINGS, MT • BIRMINGHAM, AL • CHARLESTON, WV • CLARKSBURG, WV • CLEVELAND, OH • DENVER, CO • GOLDEN, CO • HENDERSON, KY •
MIDDLESBORO, KY • MOBILE, AL • NEW ORLEANS, LA • NORFOLK, VA • PIKEVILLE, KY • VANCOUVER, B.C. CAN.

COMBUSTIBLES DATA SHEET

SITE ABMA - SITE A

Crucible Number	Sample Origin	Crucible Weight grams	Crucible & Sample Weight Post 110°C gms	Sample Weight grams	Post 750°C grams	Δ Weight grams	% Combustibles
1	Multi OUT Test #3 8/11/77 AVG.	3.6806	4.0303	.3495	3.9282	.0920	26.3
		3.6808	4.0302		3.9282		
		3.6807	4.0303		3.9382		
		3.6807	4.0302		3.9282		
2	Multi OUT Test #4 8/17/77 AVG.	3.9724	4.3050	.3326	4.2077	.0972	29.2
		3.9725	4.3050		4.2078		
		3.9724	—		4.2079		
		3.9724	4.3050		4.2078		
3	Multi OUT Test #5 8/18/77 AVG.	3.6681	4.0197	.3520	3.8874	.1324	37.6
		3.6681	4.0204		3.8878		
		3.6682	4.0203		3.8878		
		3.6681	4.0201		3.8877		
4	Multi OUT Test #6 AVG.	3.7105	4.1554	.4448	3.9811	.1741	39.1
		3.7106	—		3.9813		
		3.7106	—		3.9814		
		3.7106	4.1554		3.9813		
6	Multi OUT Test #10 8/24/77 AVG.	3.7397	3.9648	.2253	3.9197	.0453	20.1
		3.7398	3.9651		3.9199		
		3.7397	3.9650		3.9197		
		3.7397	3.9650		3.9197		
7	Multi OUT Test #15 8/27/77 AVG.	3.7833	4.0707	.2874	3.9629	.1080	37.5
		3.7836	4.0709		3.9628		
		3.7833	4.0708		3.9627		
		3.7834	4.0708		3.9628		
8	Multi OUT Test #16 8/30/77 AVG.	3.8303	4.0071	.1769	3.9692	.0379	21.4
		3.8304	4.0074		3.9693		
		3.8302	4.0072		3.9694		
		3.8303	4.0072		3.9693		
1	BLR OUT Test #21 9/23/77 AVG.	18.4210	22.7130	4.2931	19.3774	3.365	77.7
		18.4210	22.7141		19.3779		
		18.4211	22.7152		19.3776		
		18.4210	22.7141		19.3776		
2	BLR OUT Test #21 AVG.	18.1393	23.3955	5.2583	19.8804	3.5168	66.9
		18.1391	23.3978		19.8809		
		18.1392	23.3992		19.8808		
		18.1392	23.3975		19.8807		
3	BLR OUT Test #22 9/23/77 AVG.	18.5968	24.6902	6.0947	20.2473	4.4437	72.9
		18.5964	24.6912		20.2478		
		18.5966	24.6924		20.2475		
		18.5966	24.6913		20.2476		
4	BLR OUT Test #22 AVG.	18.0836	26.7754	8.6951	22.5908	4.1878	48.2
		18.0837	26.7799		22.5901		
		18.0838	26.7805		22.5909		
		18.0837	26.7788		22.5909		

COMBUSTIBLES DATA SHEET

SITE ABMA - SITE A

Crucible Number	Sample Origin	Crucible Weight grams	Crucible & Sample Weight Post 110°C gms	Sample Weight grams	Post 750°C grams	Δ Weight grams	% Combustibles
5	Test #23 AVG.	18.3872	24.1026	5.7163	21.6063	2.4962	43.7
		18.3872	24.1032		21.6069		
		18.3873	24.1045		21.6069		
		18.3872	24.1035		21.6067		
6	Test #24 AVG.	17.6397	22.6718	4.4345	19.3797	2.6941	60.8
		17.6395	22.6752		19.3800		
		17.6396	22.6751		19.3802		
		17.6396	22.6741		19.3800		
5	Test #28 AVG.	18.3875	25.7586	7.3711	21.0780	4.6806	63.5 65.8
		18.3875	25.7586		21.0781		
		18.3875	25.7587		21.0780		
		18.3875	25.7586		21.0780		
9	Test #28 AVG.	18.0970	26.5611	8.4642	20.8225	5.7327	67.8
		18.0970	26.5612		20.8225		
		18.0971	26.5614		20.8226		
		18.0970	26.5612		20.8225		
2	Test #29 AVG.	18.5973	22.1154	3.5182	19.9914	2.1240	60.3 54.6
		18.5973	22.1155		19.9916		
		18.5974	22.1152		19.9916		
		18.5973	22.1155		19.9915		
3	Test #29 AVG.	18.1396	26.4199	8.2802	22.0977	4.3222	52.2
		18.1397	26.4198		22.0978		
		18.1397	26.4199		22.0975		
		18.1397	26.4199		22.0977		
6	Test #21 AVG.	17.6399	20.7708	3.1309	18.7925	1.9783	63.2
		17.6400	20.7708		18.7926		
		17.6402	20.7710		18.7926		
		17.6400	20.7709		18.7926		
7	Test #24 AVG.	18.5167	26.4028	7.8860	22.9883	3.4146	43.3
		18.5168	26.4027		22.9882		
		18.5169	26.4029		22.9883		
		18.5168	26.4028		22.9883		
4	Test #26A AVG.	18.0836	24.2442	6.1606	21.0224	3.2219	52.3
		18.0837	24.2442		21.0223		
		18.0837	24.2444		21.0224		
		18.0837	24.2443		21.0224		
12	Test #26B AVG.	3.9450	4.3681	4.2335	4.2379	.1206	30.8
		3.9450	4.3684		4.2379		
		3.9451	4.3687		4.2380		
		3.9450	4.3685		4.2379		
	AVG.						

CARBON ANALYSIS

Crucible Number	Sample Origin	Crucible Weight	Crucible + Sample Wt. Post 110°C	Sample Weight	Post 750°C	Residue Weight	% Ash	Post 950°C Weight	Δ Weight	% Volatiles	Fixed Carbon FC= 100-%V-%A
7	Test #36	18.5176	22.3623	3.8441	19.5303			19.4933	.0271	0.9	39.1
		18.5175	22.3622		19.5303			19.4932			
		18.5175	22.3622		19.5304			19.4930			
		18.5175	22.3622		19.5303			19.4932			
6	Test #37	17.6414	23.1902	5.5489	18.6639			18.6237	.0403	0.7	33.8
		17.6414	23.1904		18.6641			18.6236			
		17.6415	23.1904		18.6641			18.6237			
		17.6414	23.1903		18.6640			18.6237			
2	Test #38	18.1417	19.7686	1.6270	19.1389			19.1069	.0320	1.9	36.9
		18.1415	19.7684		19.1391			19.1069			
		18.1414	19.7684		19.1389			19.1070			
		18.1415	19.7685		19.1390			19.1069			
9	Test #39	18.0988	21.6488	3.5501	19.1206			19.0819	.0385	1.0	51.9
		18.0987	21.6487		19.1208			19.0826			
		18.0984	21.6486		19.1208			19.0824			
		18.0986	21.6487		19.1207			19.0823			
5	Test #36	18.3890	23.3909	5.0018	21.3926	2.0039	60.0				
		18.3890	23.3908		21.3927						
		18.3891	23.3909		21.3933						
		18.3890	23.3908		21.3929						
3	Test #37	18.5980	22.7596	4.1616	21.3275	2.7298	65.5				
		18.5981	22.7597		21.3281						
		18.5981	22.7597		21.3281						
		18.5981	22.7597		21.3279						
11	Test #38	18.6156	19.8482	1.2327	19.2700	.7554	61.2				
		18.6154	19.8482		19.3713						
		18.6155	19.8481		19.3714						
		18.6155	19.8482		19.3709						
4	Test #39	18.0848	20.8113	2.7264	19.3698	1.2856	47.1				
		18.0847	20.8111		19.3708						
		18.0848	20.8111		19.3707						
		18.0848	20.8112		19.3704						
			</								

KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. A

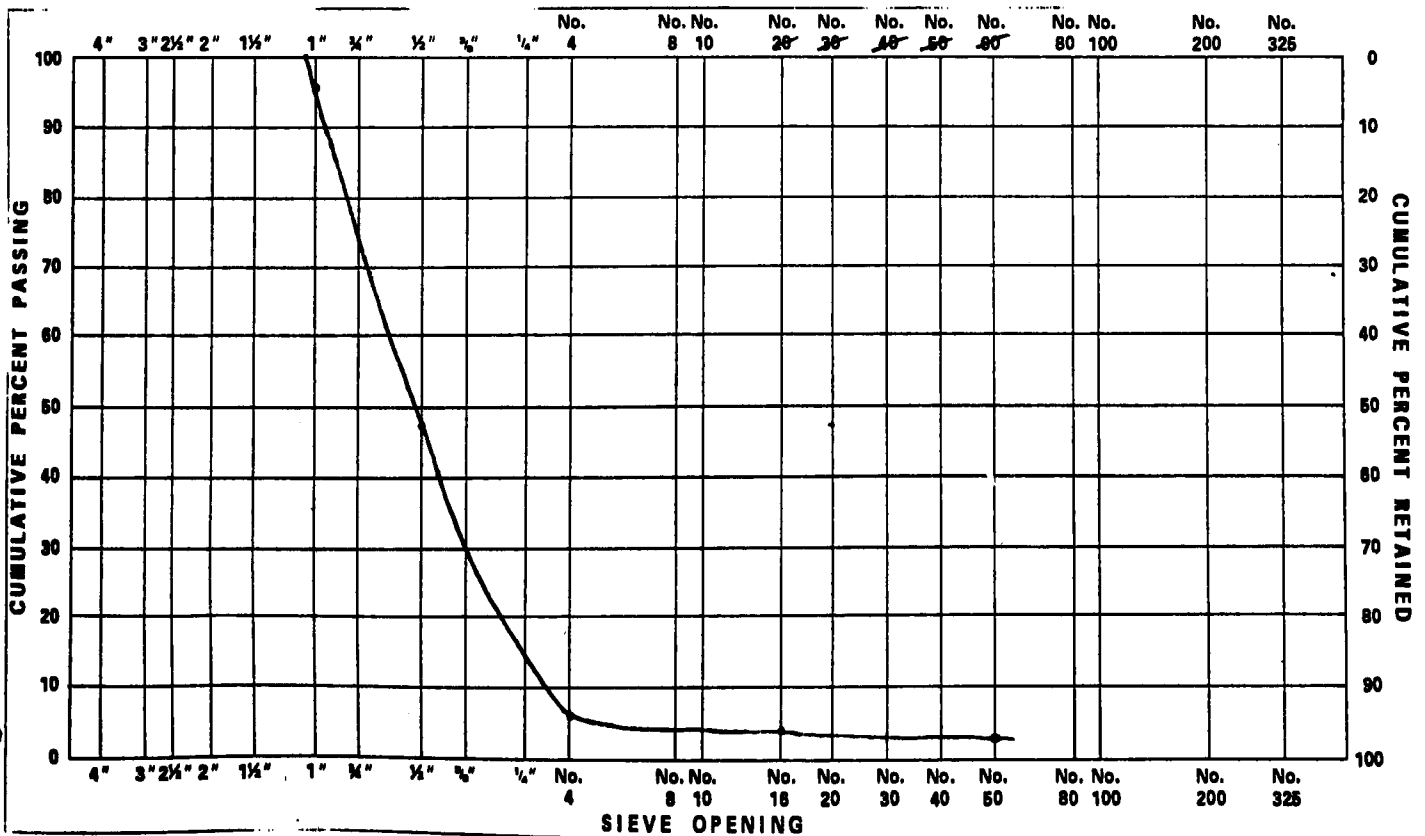
DATE SAMPLE TAKEN Aug 9 1977

TEST SITE ABMA - SITE A

TEST PERFORMED BY PLL

SAMPLE IDENTIFICATION Conveyor Belt grab sample

Screen Size Passing	Tare Weight (gm)	Gross Weight (gm)	Net Weight (gm)	Percent (%)	Cumulative Weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
Top	400.4	529.0	158.6	3.60	4563.2	100.00	
1"	400.4	2502.0	2260.2	47.71	4404.6	96.52	
1/2"	400.4	2297.6	1897.2	43.07	2144.4	46.99	
*4	400.4	452.5	52.1	1.18	2472	5.42	
*16	400.4	453.4	53.0	1.20	195.1	4.28	
*50	400.4	542.5	142.1	3.23	142.1	3.11	



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. B

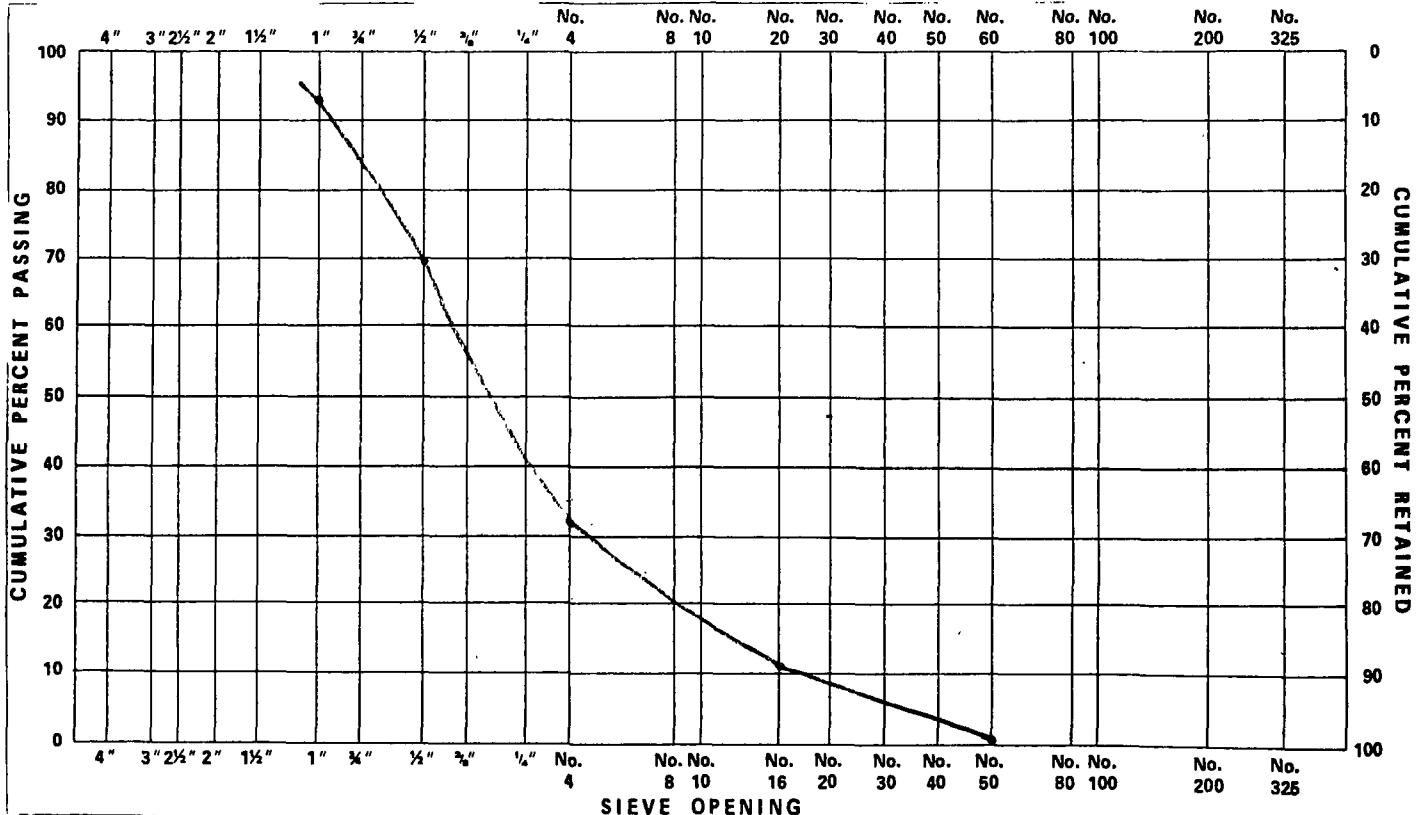
DATE SAMPLE TAKEN Aug 9 1977

TEST SITE ABMA - SITE A

TEST PERFORMED BY PLL

SAMPLE IDENTIFICATION FEEDER #4

Screen Size Passing	Tare Weight (gm)	Gross Weight (gm)	Net Weight (gm)	Percent (%)	Cumulative Weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
Top	168.7	553.3	384.6	7.15	5376.2	100.00	
1"	168.7	1402.0	1233.3	22.94	4991.6	92.85	
1/2"	168.7	2193.3	2024.6	37.66	3758.3	69.91	
#4	168.7	1321.0	1152.3	21.43	1733.7	32.25	
#16	168.7	729.3	560.6	10.43	581.4	10.82	
#50	168.7	189.5	20.8	0.39	20.8	0.39	



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. C

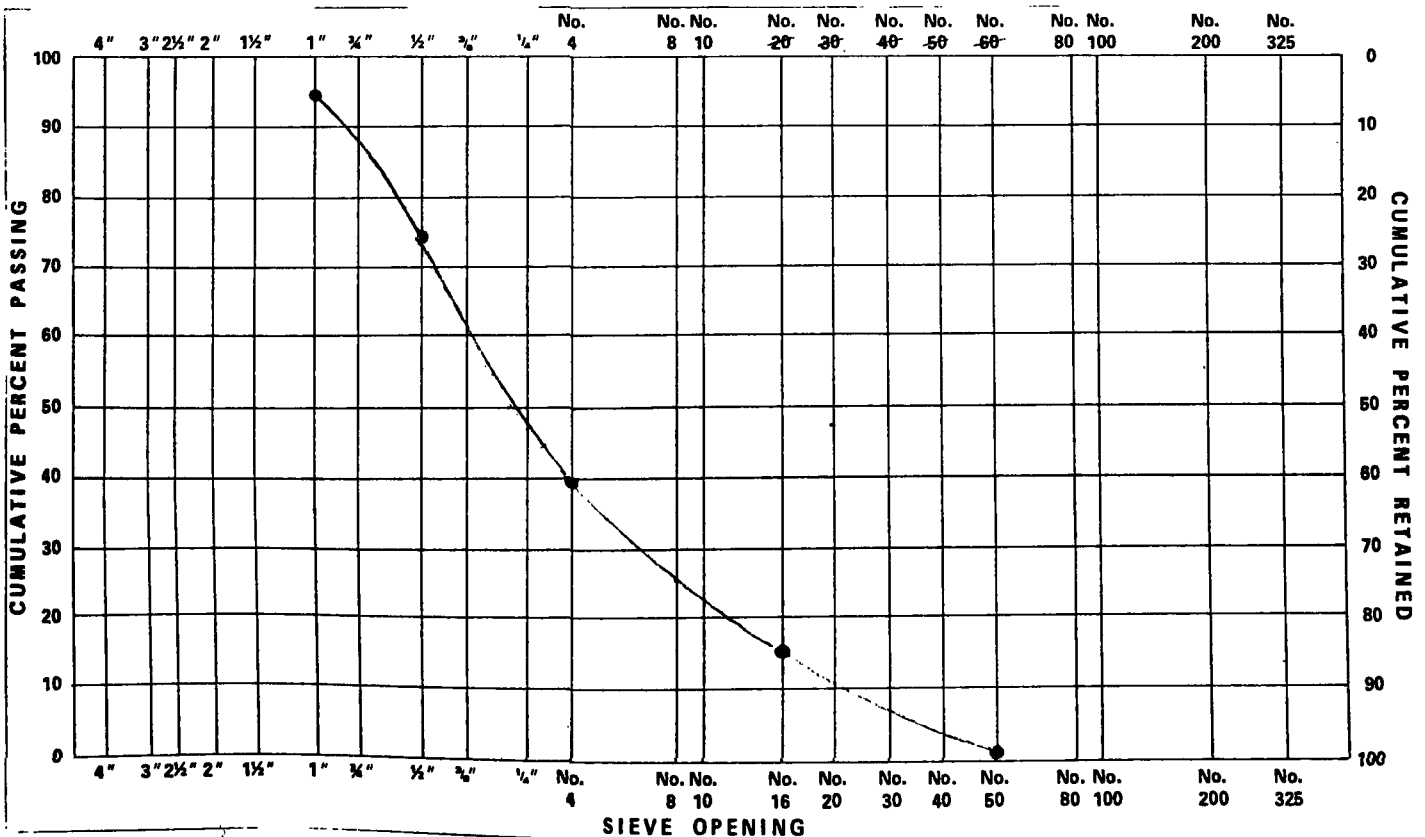
DATE SAMPLE TAKEN 8/24/77

TEST SITE ABMA - SITE A

TEST PERFORMED BY WJS

SAMPLE IDENTIFICATION FROM BELT

Screen Size Passing	Tare Weight (gm)	Gross Weight (gm)	Net Weight (gm)	Percent (%)	Cumulative Weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
TOP	168.0	455.7	287.7	5.2	5566.8	100.0	1
1"	168.0	1316.5	1148.5	20.6	5779.1	94.8	2
1/2"	168.0	2048.4	1920.4	34.5	4130.6	74.2	3
#4	168.0	1530.5	1368.5	24.6	2210.2	39.7	6
#16	168.0	968.7	800.7	14.1	841.7	15.1	15
#50	168.0	209.0	41.0	0.7	41.0	0.7	—



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. D

DATE SAMPLE TAKEN 11 Sep 77

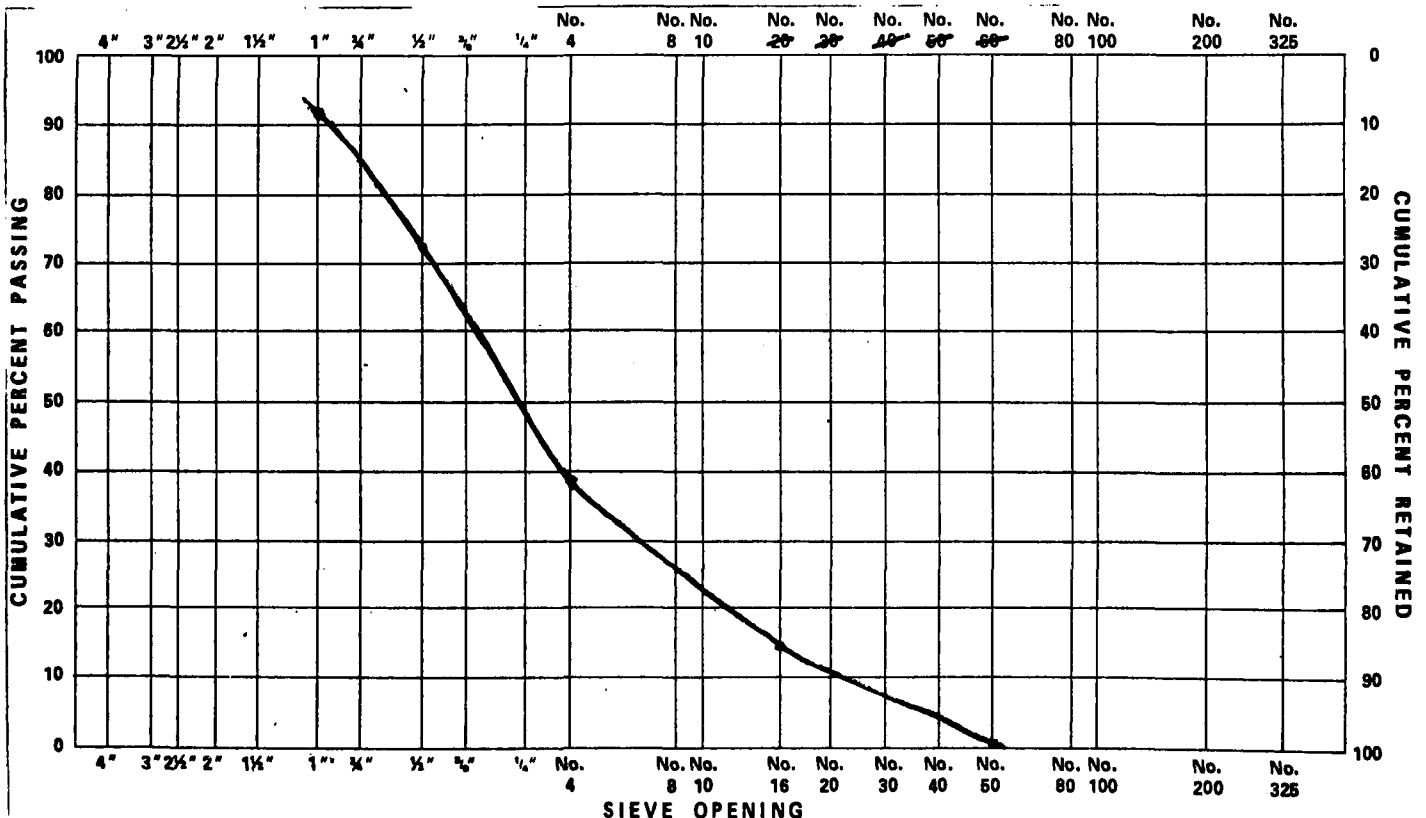
TEST SITE ABMA-SITE A

TEST PERFORMED BY Pat

SAMPLE IDENTIFICATION From conveyor belt

Screen Size Passing	Tare Weight (gm)	Gross Weight (gm)	Net Weight (gm)	Percent (%)	Cumulative Weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
TOP	168.1	760.3	592.2	7.86	7529.6	100.00	1
1"	168.1	1658.9	1490.8	19.80	6937.4	92.14	2
1/2"	168.6	1663.5 + 1203.6	2529.9	33.60	5446.6	72.34	5
#4	168.5	2055.0	1886.5	25.05	2916.7	38.74	10
#16	168.5	1147.2	978.7	13.00	1030.2	13.69	20
#50	168.5	* 220.0	51.5	0.68	51.5	0.69	—

* again, coal not + would not pass thru #50 sieve



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. -

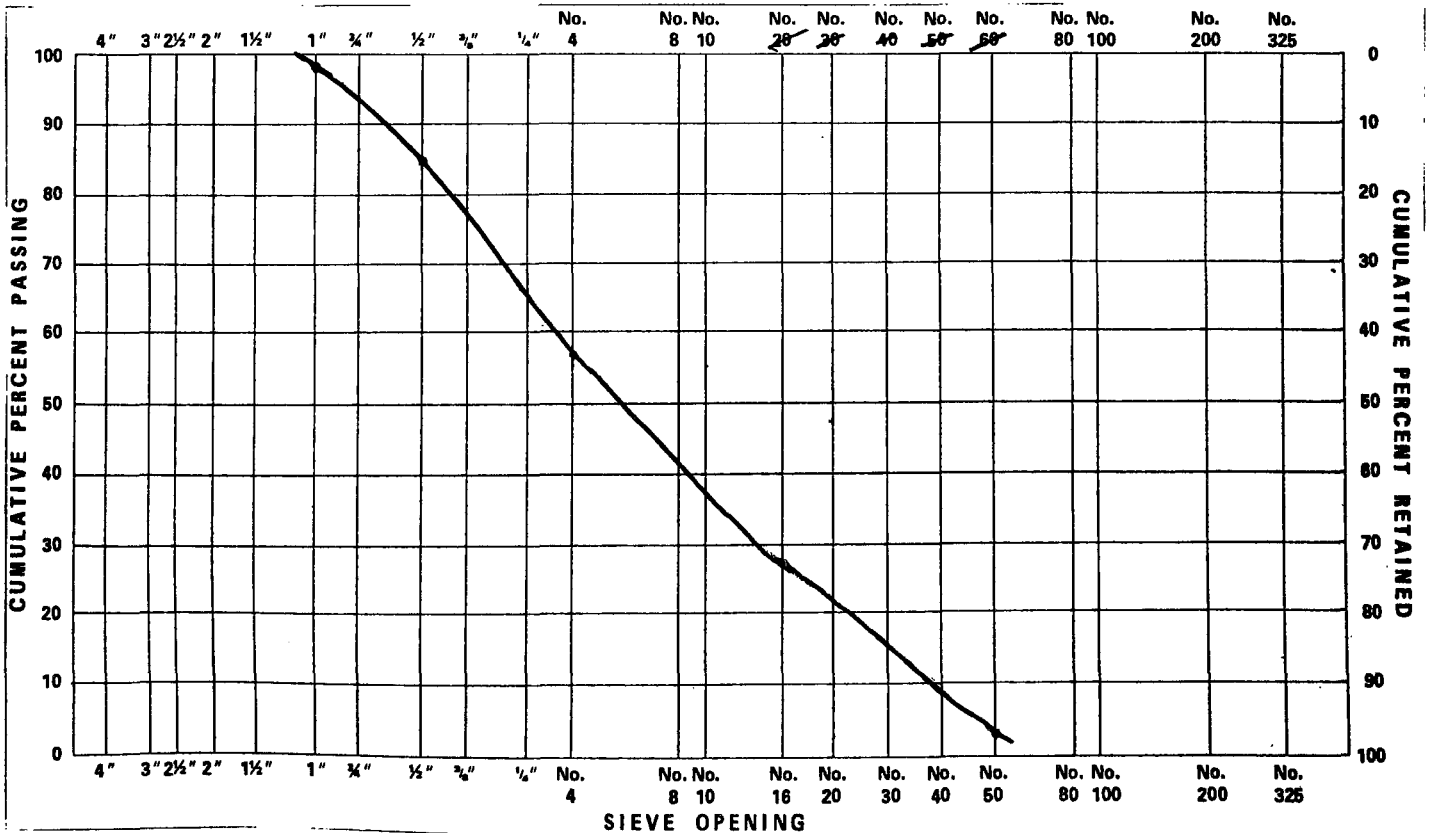
DATE SAMPLE TAKEN 9-15-77

TEST SITE ARMA-SITE A

TEST PERFORMED BY PLL, K

SAMPLE IDENTIFICATION Conveyor Belt

Screen Size Passing	Tare Weight (gm)	Gross Weight (gm)	Net Weight (gm)	Percent (%)	Cumulative Weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
TOT	168.7	222.0 334.4	219.0	2.40	9109.1	100.00	1
1"	168.7	786.9 717.8	1167.3	12.81	8890.1	97.60	2
1/2"	168.7	1675.7 1225.4	2563.7	28.14	7722.8	84.79	5
#4	168.7	1794.4 1249.7	2706.7	29.71	5159.1	56.65	10
#16	168.7	1513.6 1052.7	2228.9	24.47	2452.4	26.94	-
#50	168.7	284.7 276.2	223.5	2.45	223.5	2.47	-



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. _____

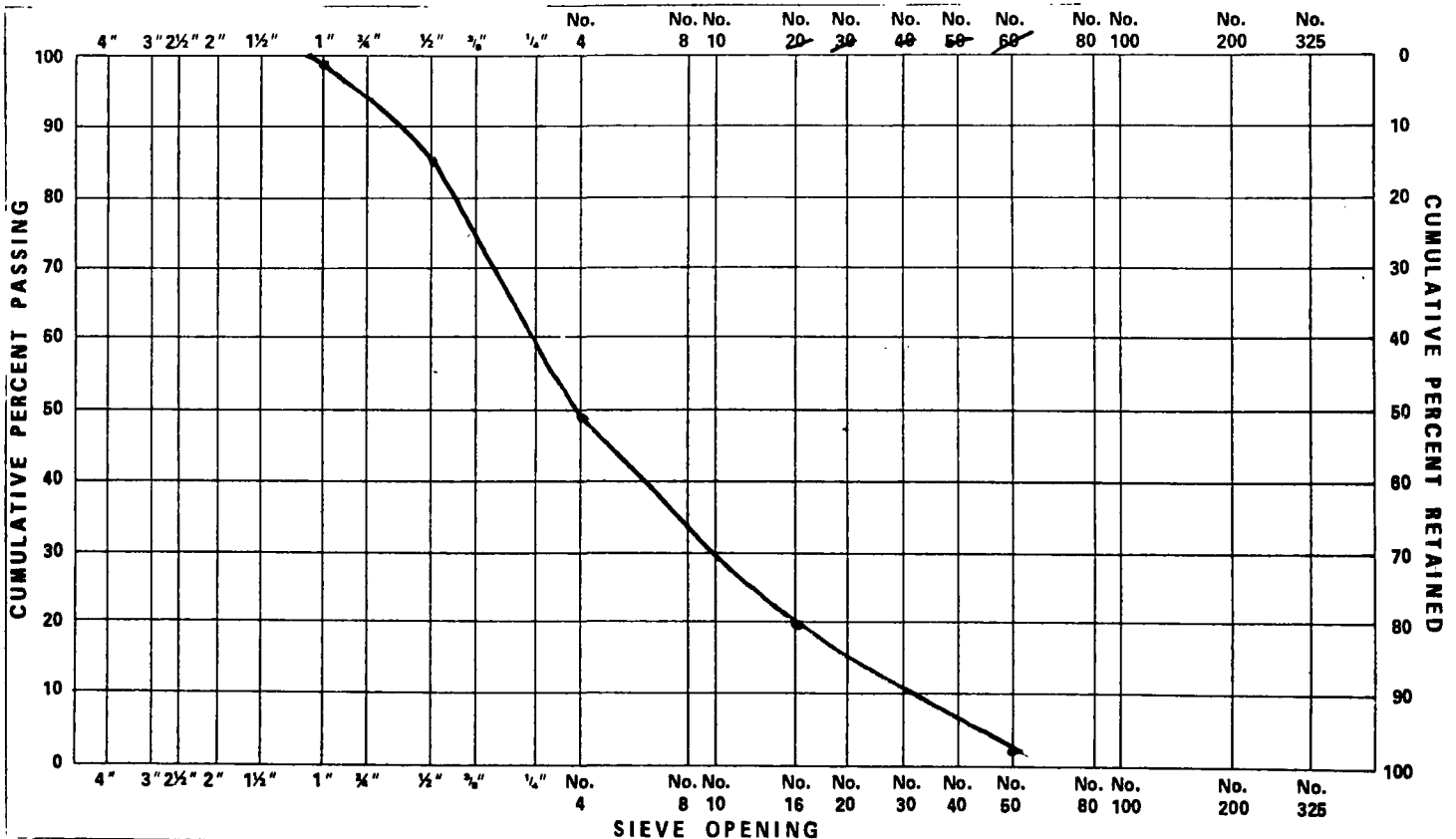
DATE SAMPLE TAKEN 9-15-77

TEST SITE ABMA - SITE A

TEST PERFORMED BY PLL, K

SAMPLE IDENTIFICATION FEEDERS

Screen Size Passing	Tare Weight (gm)	Gross Weight (gm)	Net Weight (gm)	Percent (%)	Cumulative Weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
TOP	168.9	191.3 259.7	113.2	1.49	7595.0	100.00	1
1"	168.9	528.5 839.0	1029.7	13.56	7481.8	98.51	2
$\frac{1}{2}$ "	168.9	1441.9 1620.0	2724.1	35.87	6452.1	84.95	5
#4	168.9	1324.8 1239.0	2225.2	29.30	3728.0	49.08	10
#16	168.9	819.6 859.2	1341.0	17.66	1502.8	19.78	—
#50	168.9	330.7	161.8	2.13	161.8	2.12	—



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. 21

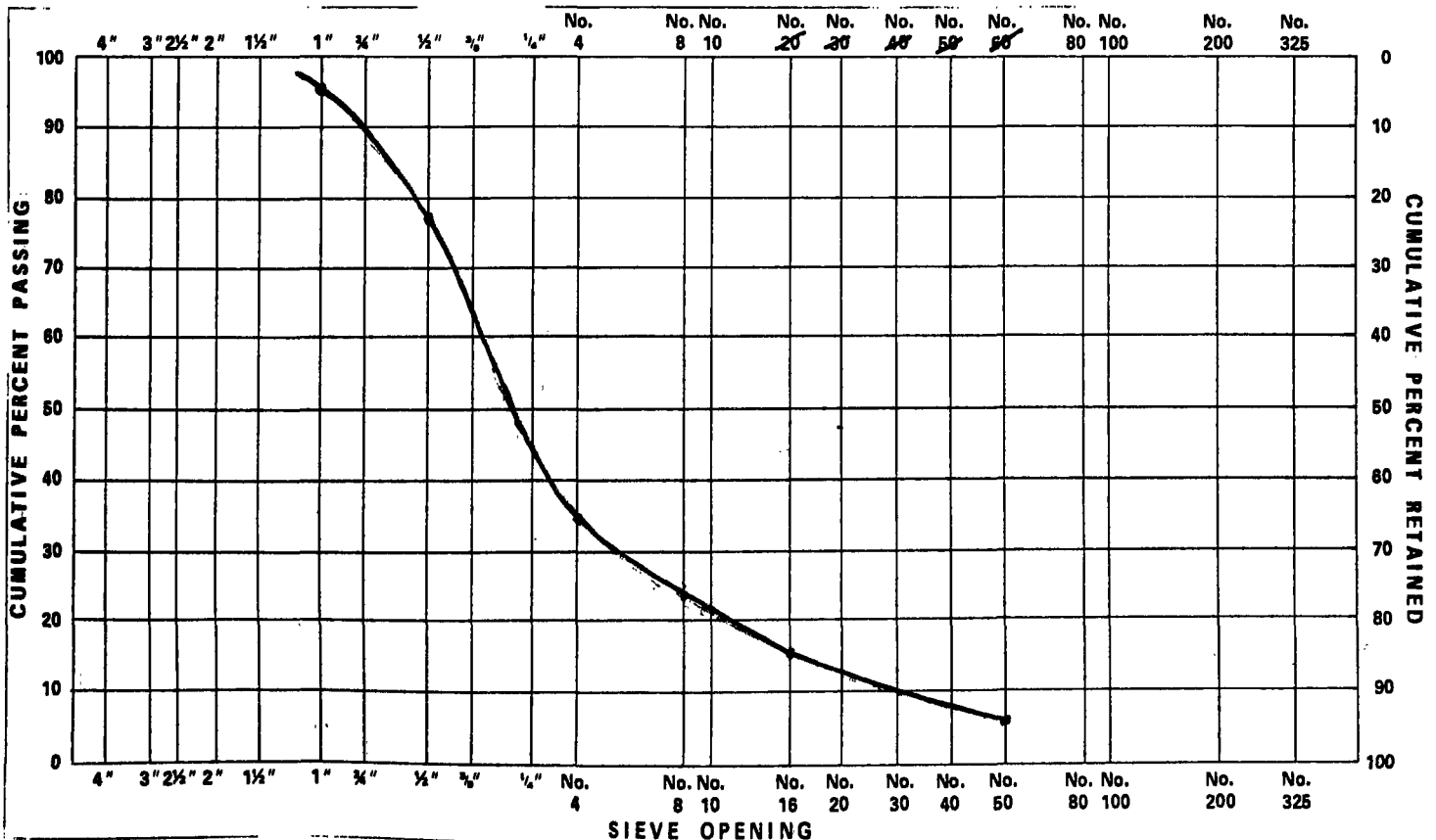
DATE SAMPLE TAKEN 9-23-77

TEST SITE ABMA-SITE A

TEST PERFORMED BY PLL, JLB

SAMPLE IDENTIFICATION KEMMERER COAL

Screen Size Passing	Tare Weight (gm)	Gross Weight (gm)	Net Weight (gm)	Percent (%)	Cumulative Weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
TOP	169.8	339.6 224.0	224.0	4.12	5438.4	100.00	1
1"	169.8	879.8 458.7	993.9	18.28	5214.4	95.88	2
1/2"	169.8	1397.8 1331.8	2390.0	43.95	4220.5	77.60	5
#4	169.8	1054.2 280.3	994.9	18.29	1830.5	33.65	10
#16	169.8	475.6 349.2	485.2	8.92	835.6	15.36	15
#50	169.8	520.2	350.4	6.44	350.4	6.44	—



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. 22

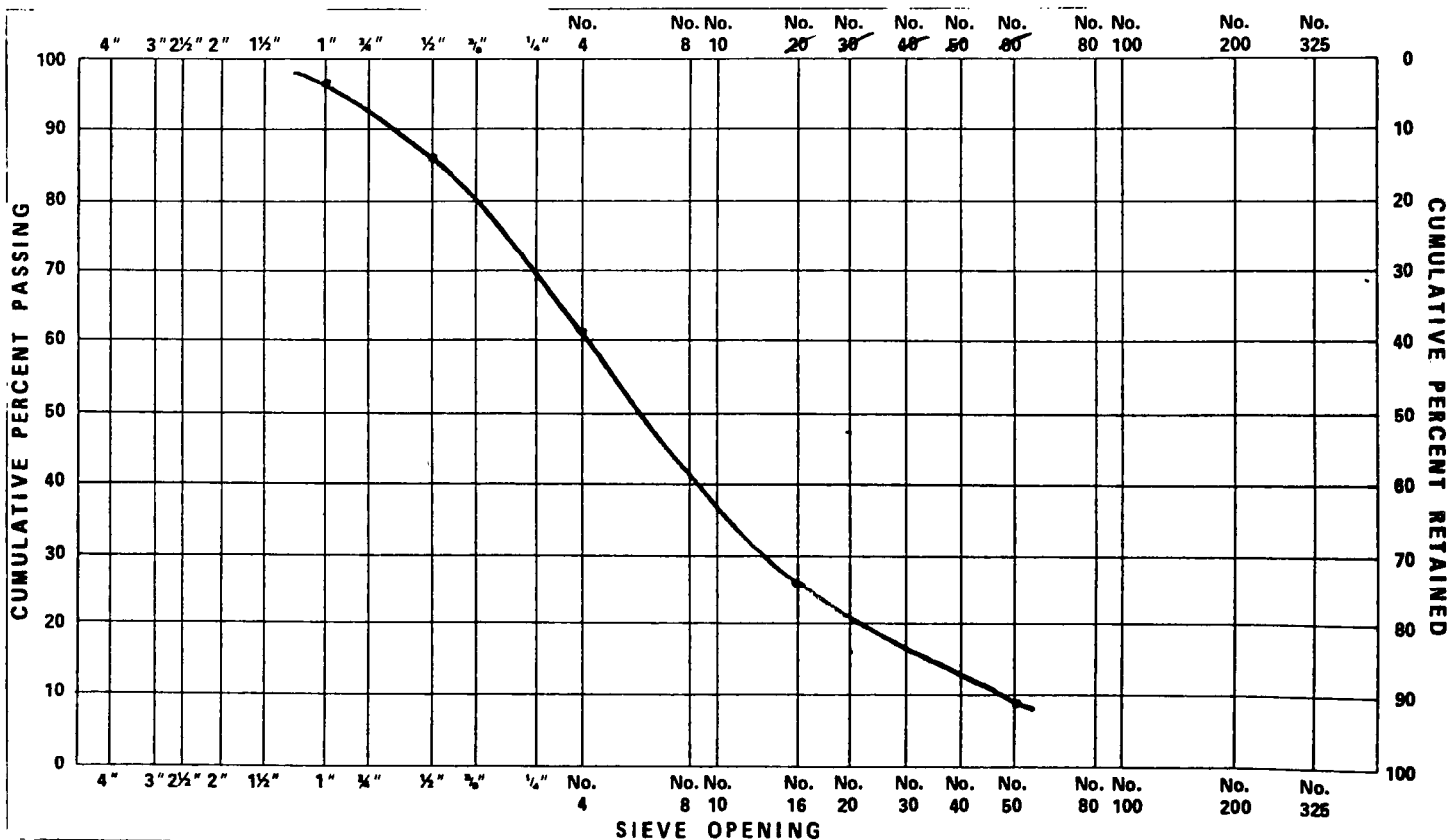
DATE SAMPLE TAKEN 9-23-77

TEST SITE ABMA-SITE A

TEST PERFORMED BY PLL, J03

SAMPLE IDENTIFICATION KEMMERER COAL

Screen Size Passing	Tare Weight (gm)	Gross Weight (gm)	Net Weight (gm)	Percent (%)	Cumulative Weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
Top	169.8	269.9	100.1	2.76	3631.7	100.00	1
1"	169.8	552.5	382.7	10.54	3531.6	97.24	2
2"	169.8	1096.5	926.7	25.52	3148.9	86.70	5
#4	169.8	1438.8	1269.0	34.94	2222.2	61.18	10
#16	169.8	772.8	609.0	16.77	953.2	26.24	15
#20	169.8	514.0	344.2	9.48	344.2	9.47	—



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. 23

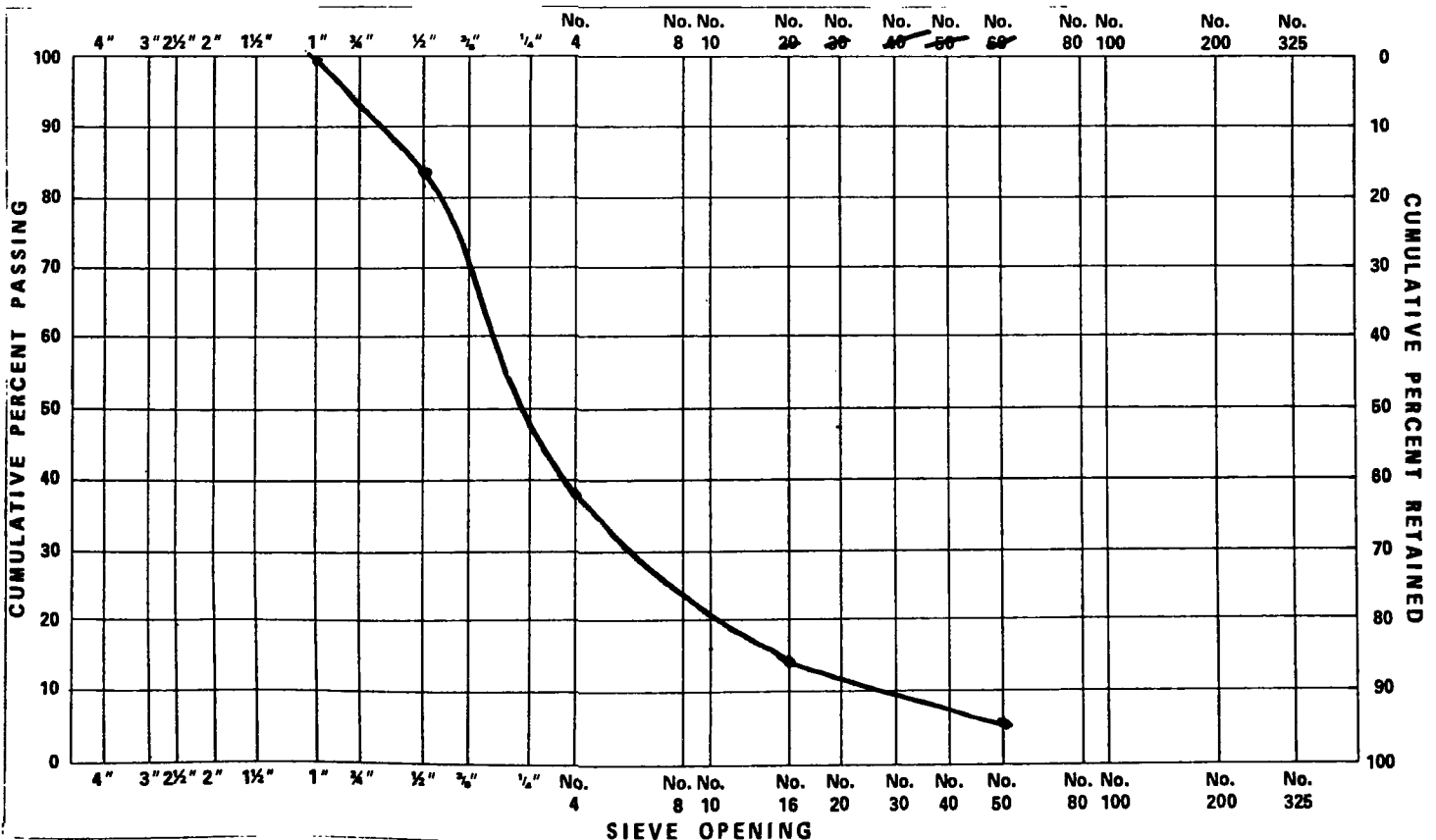
DATE SAMPLE TAKEN 9-24-77

TEST SITE ABMA-SITE A

TEST PERFORMED BY PLL, JOB

SAMPLE IDENTIFICATION KEMMEKER COAL

Screen Size Passing	Tare Weight (gm)	Gross Weight (gm)	Net Weight (gm)	Percent (%)	Cumulative Weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
Top	169.8	210.1	40.3	0.88	4572.7	100.00	1
1"	169.8	908.1	738.3	16.15	4532.4	99.12	2
1/2"	169.8	2220.5	2050.7	44.85	3794.1	82.97	5
#4	169.8	1317.9	1148.1	25.11	1743.4	38.12	10
#16	169.8	510.5	340.7	7.45	595.3	13.01	15
#50	169.8	424.4	254.6	5.57	254.6	5.56	—



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. 24

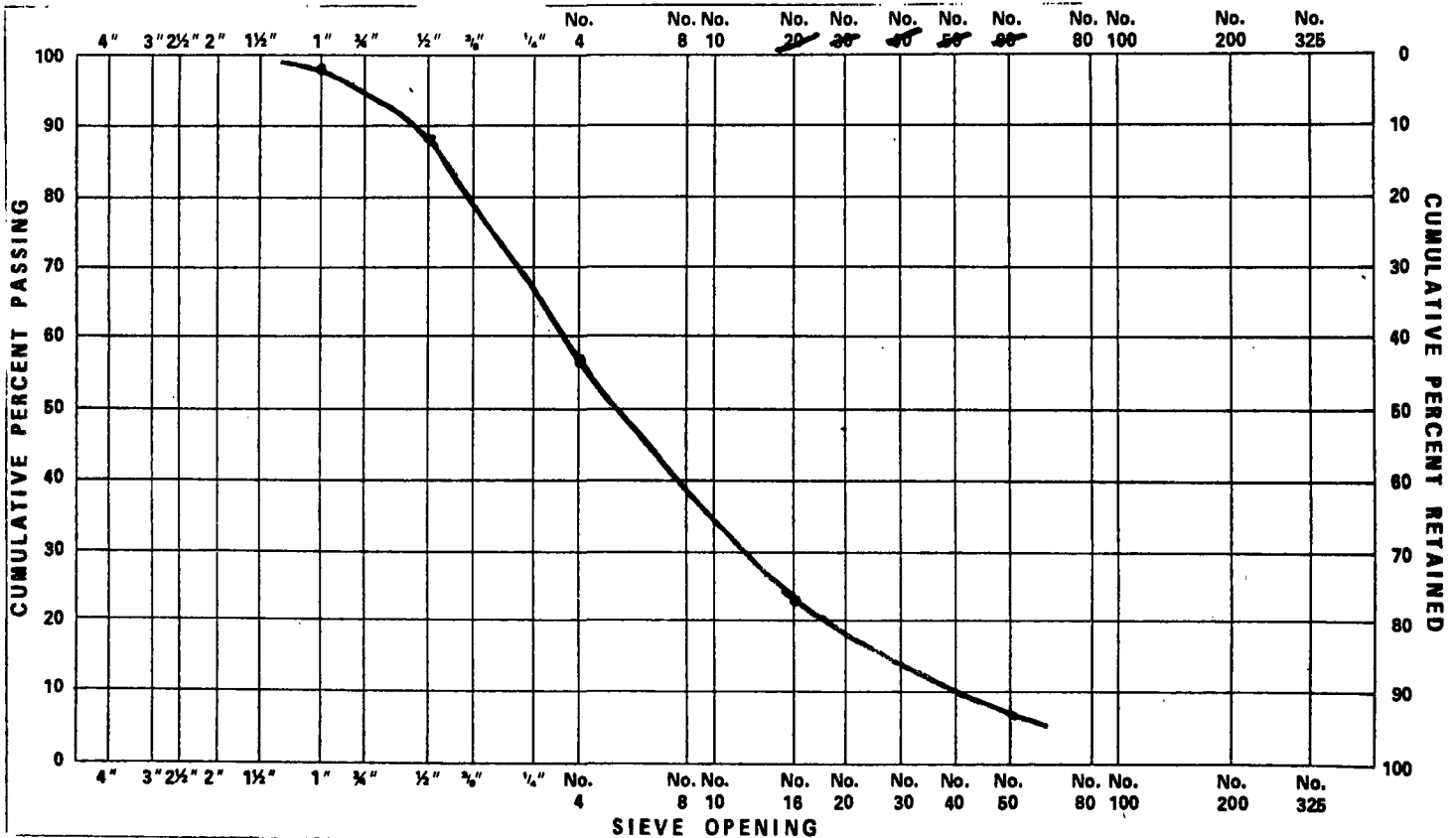
DATE SAMPLE TAKEN 9-24-77

TEST SITE ABMA-SITE A

TEST PERFORMED BY PLL, JOB

SAMPLE IDENTIFICATION KEMMERER COAL

Screen Size Passing	Tare Weight (gm)	Gross Weight (gm)	Net Weight (gm)	Percent (%)	Cumulative Weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
Top	169.8	201.4 250.2	112.0	1.80	6226.4	100.00	1
1"	169.8	410.1 576.3	646.8	10.39	6114.4	98.20	2
1/2"	169.8	834.4 1437.0	1931.8	31.03	5467.6	87.81	5
#4	169.8	841.3 1644.4	2146.1	34.47	3535.8	56.78	10
#16	169.8	423.4 855.1	938.9	15.08	1389.7	22.31	15
#50	169.8	620.6	450.8	7.24	450.8	7.23	—



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. 26 A

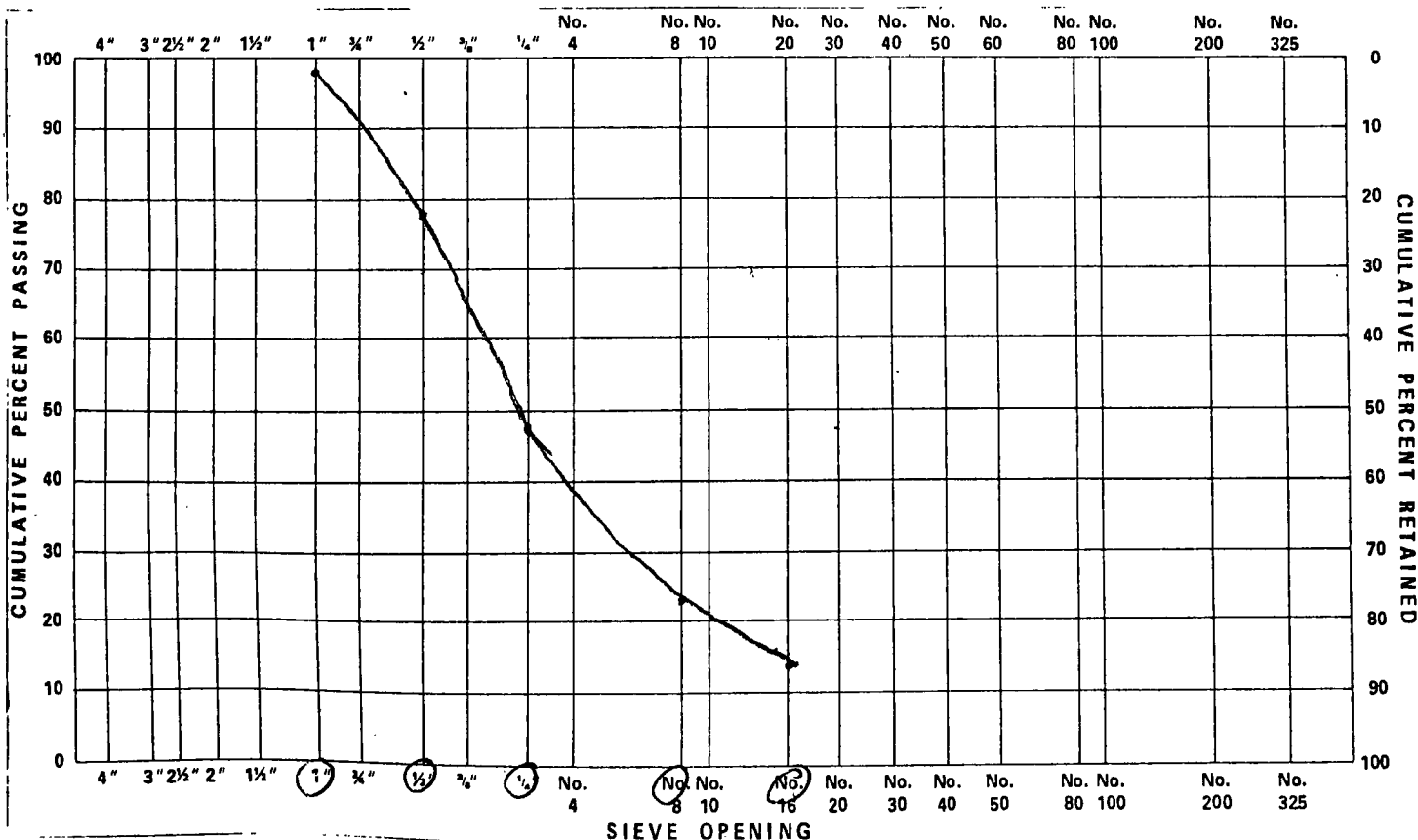
DATE SAMPLE TAKEN 6 Oct 77

TEST SITE A

TEST PERFORMED BY APR

SAMPLE IDENTIFICATION KEMMERER COAL

Screen Size Passing	Tare weight (gm)	Gross weight (gm)	Net Weight (gm)	Percent (%)	Cumulative Weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
TOP	168.8	260.7 213.1	136.2	2	7715.3	100	1
1"	168.8	1061.5 869.4	1593.3	20	7579.1	98	2
1/2"	168.8	1368.5 1333.0	2363.9	31	5985.2	78	4
1/4"	168.8	952.5 1235.1	1850.0	24	3621.9	47	8
#8	168.8	428.4 587.4	678.2	9	1771.9	23	16
#16	168.8	586.8 844.5	1093.7	14	1093.7	14	—



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. 26-B

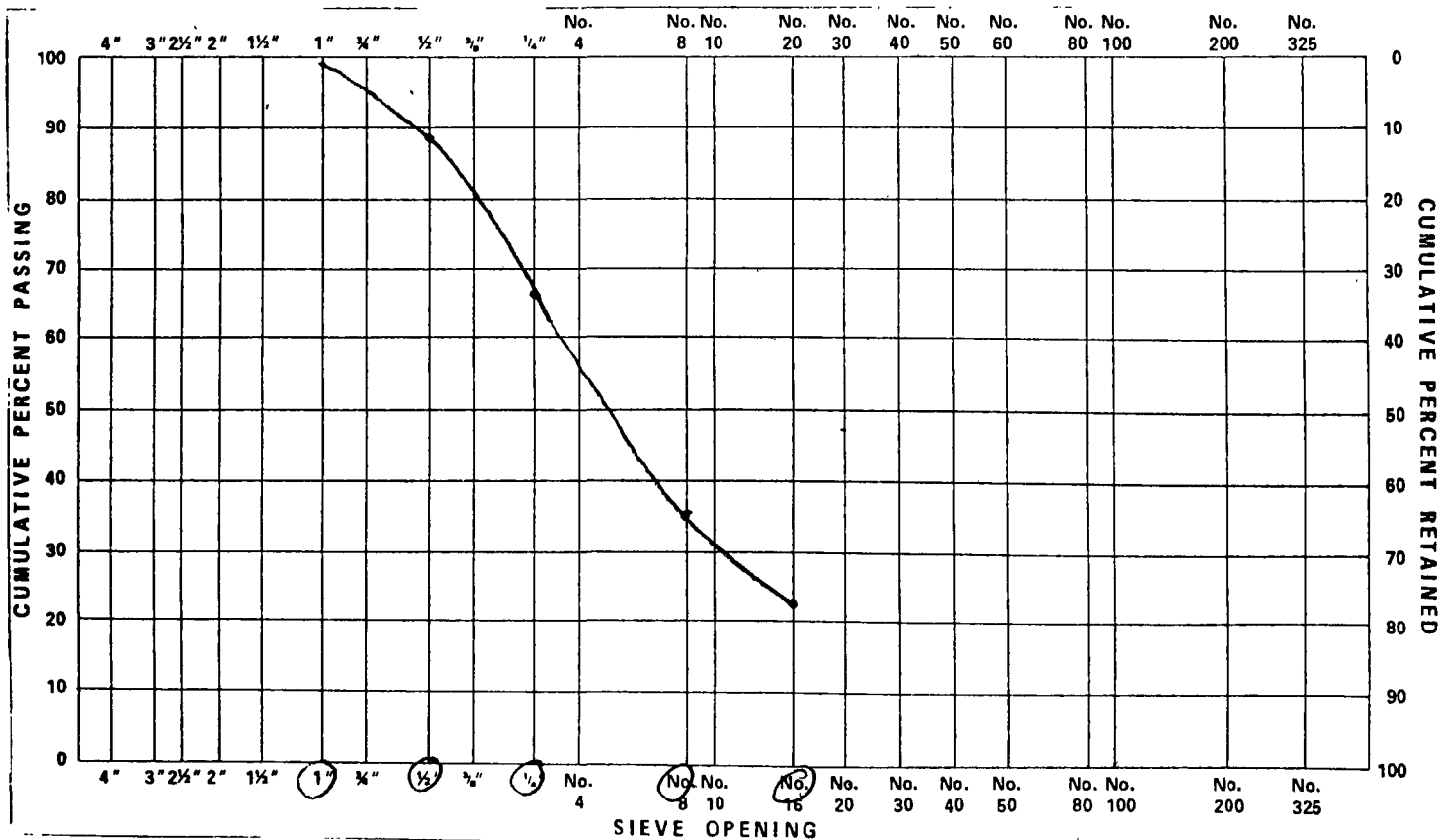
DATE SAMPLE TAKEN 10-06-77

TEST SITE A

TEST PERFORMED BY JB

SAMPLE IDENTIFICATION KEMMERER COAL

Screen Size Passing	Tare weight (gm)	Gross weight (gm)	Net weight (gm)	Percent (%)	Cumulative weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
Top	169.1	220.6 220.6	120.8	1	7611.2	100	1
1"	169.1	1572.8 535.9	770.5	10	7490.4	99	2
1/2"	169.1	1022.4 1039.5	1723.7	23	6719.9	89	4
1/4"	169.1	1381.9 1293.2	2326.9	31	4996.2	66	8
#8	169.1	708.4 651.8	1022	13	2669.3	35	16
#16	169.1	1053.9 931.6	1647.3	22	1647.3	22	-



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. 27

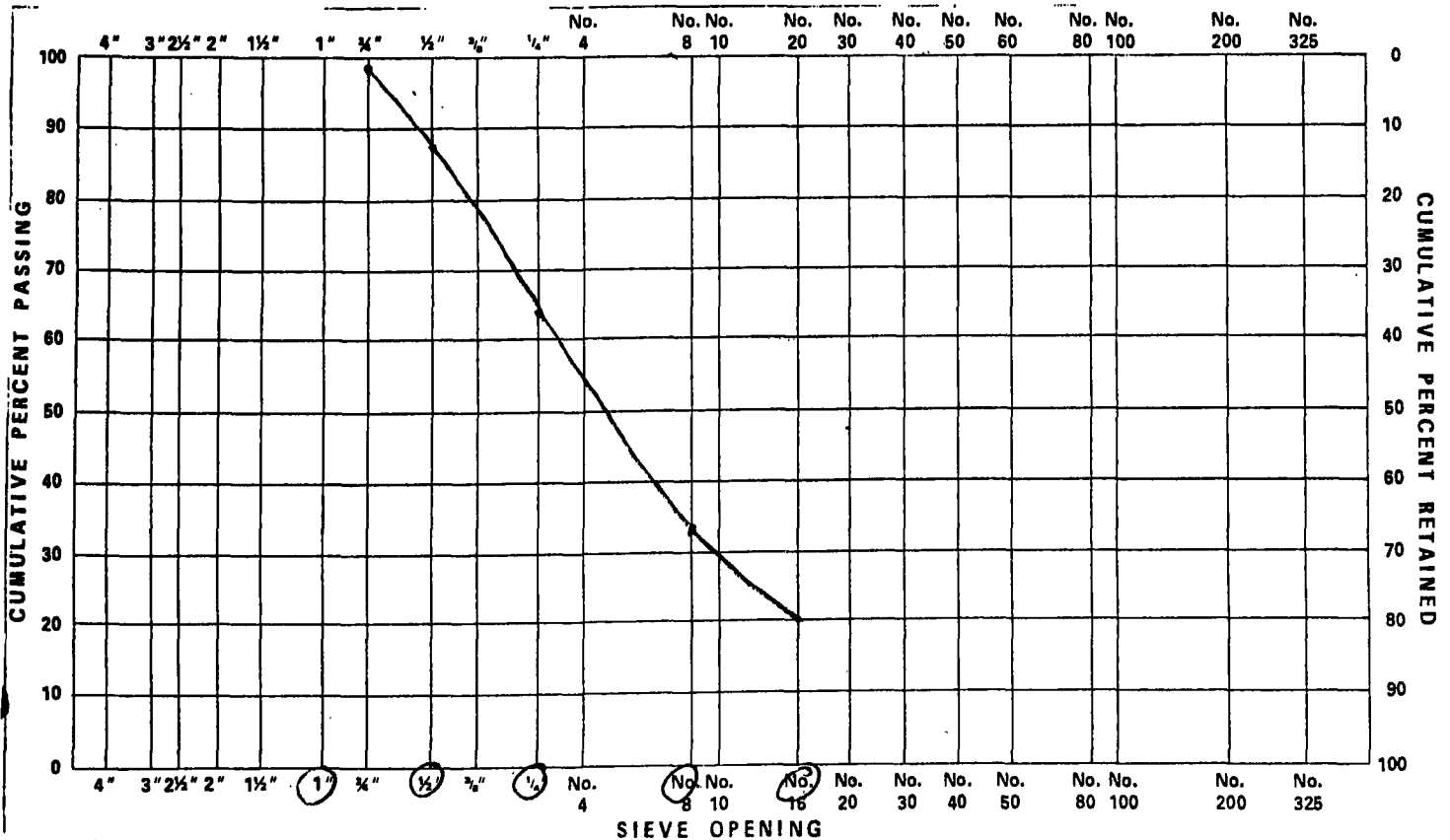
DATE SAMPLE TAKEN 10-08-77

TEST SITE A

TEST PERFORMED BY JOB

SAMPLE IDENTIFICATION KEMMERS GAL

Screen Size Passing	Tare weight (gm)	Gross weight (gm)	Net weight (gm)	Percent (%)	Cumulative weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
TOP	168.6	211.5	42.9	1	4328.9	100	1
1"	168.6	647.5	478.9	11	4286	99	2
1/2"	168.6	1212.4	1043.8	24	3807.1	88	4
3/8"	168.6	1494.2	1325.6	31	2763.3	64	8
#8	168.6	743.8	575.2	13	1437.7	33	16
#16	168.6	1031.1	862.5	20	862.5	20	—



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. 28

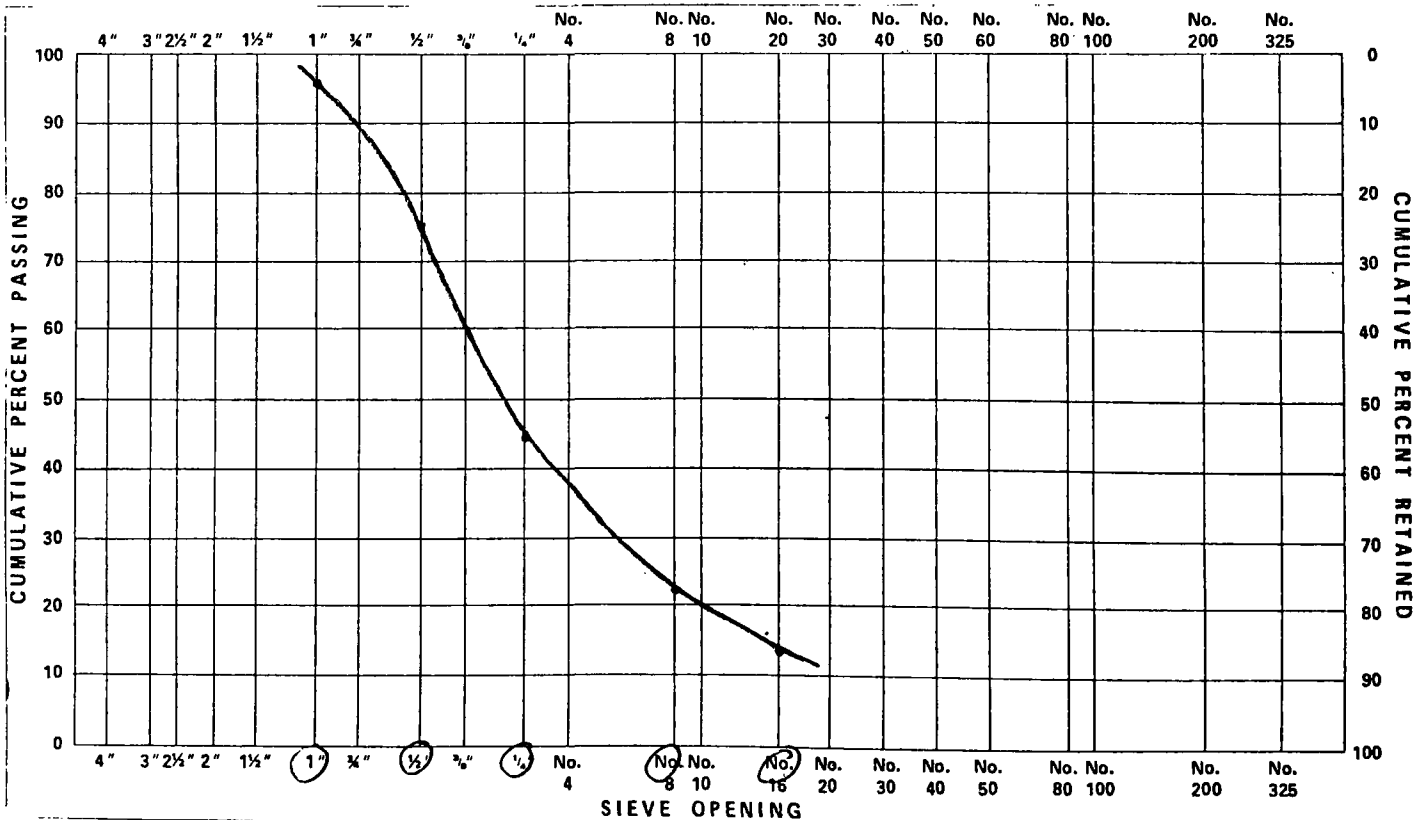
DATE SAMPLE TAKEN 10-10-77

TEST SITE A

TEST PERFORMED BY JOB

SAMPLE IDENTIFICATION KEMMERER GAL

Screen Size Passing	Tare Weight (gm)	Gross Weight (gm)	Net Weight (gm)	Percent (%)	Cumulative Weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
TOP	169.0	514.9	345.9	4.25	8143.2	100.00	1
1"	169.0	1909.5	1740.5	21.37	7797.3	95.75	2
1/2"	169.0	1739.5 1041.1	2442.6	30.00	6056.8	74.38	4
3/4"	169.0	1979.0	1810.0	22.23	3614.2	44.38	8
#8	169.0	861.6	692.6	8.51	1804.2	22.15	16
#16	169.0	1280.6	1111.6	13.65	1111.6	13.64	—



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. 29

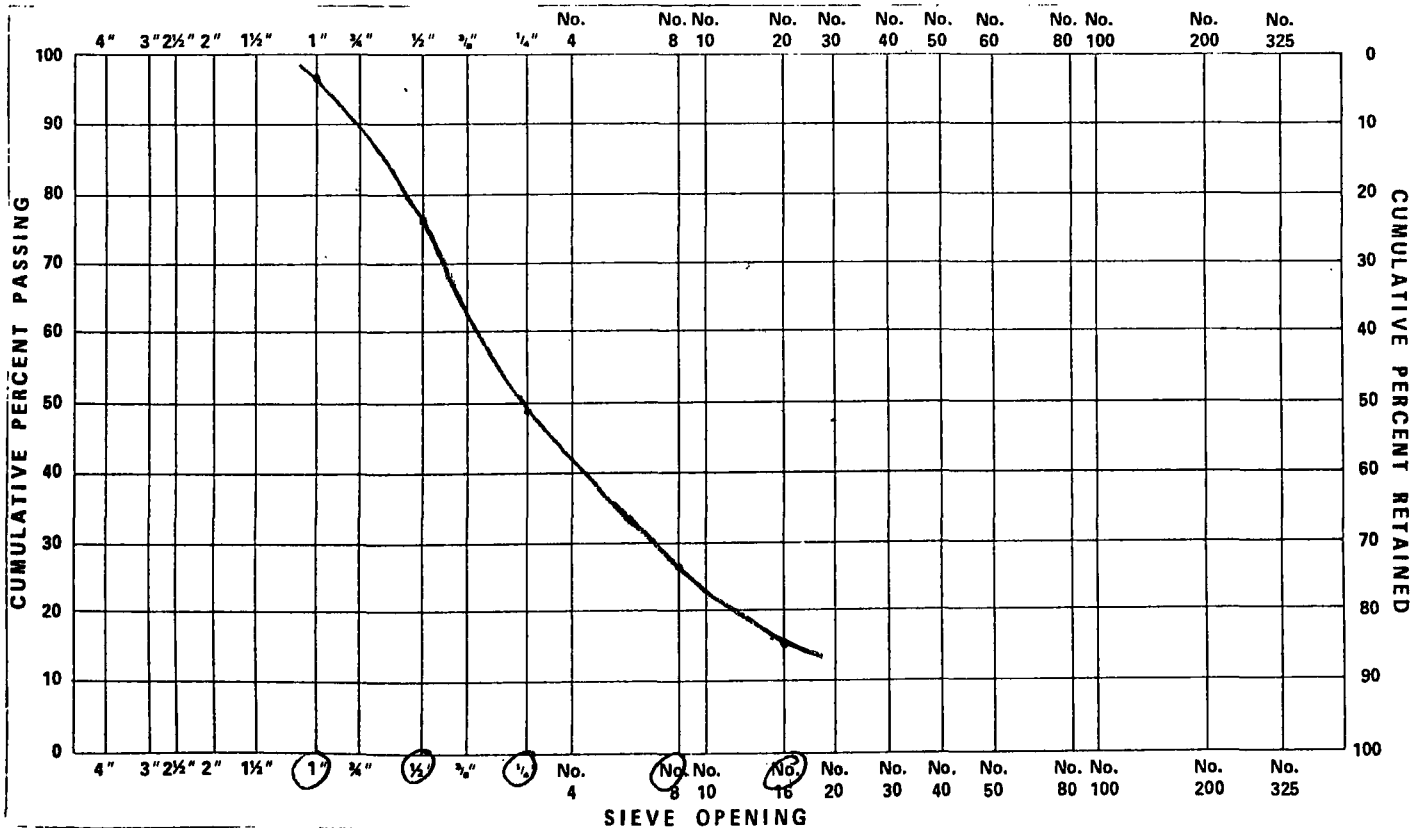
DATE SAMPLE TAKEN 10-10-77

TEST SITE A

TEST PERFORMED BY lbs

SAMPLE IDENTIFICATION KEMMERER COAL

Screen Size Passing	Tare Weight (gm)	Gross Weight (gm)	Net Weight (gm)	Percent (%)	Cumulative Weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
Top	169.0	426.7	257.7	3.37	7656.2	100.00	1
1"	169.0	1739.7	1570.7	20.51	7398.5	96.63	2
1/2"	169.0	2277.8	2108.8	27.54	5827.8	76.12	4
3/4"	169.0	1884.7	1715.7	22.41	3719.0	48.58	8
#8	169.0	967.9	798.9	10.43	2003.3	26.17	16
#16	169.0	1373.4	1204.4	15.73	1204.4	15.74	—



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. 30

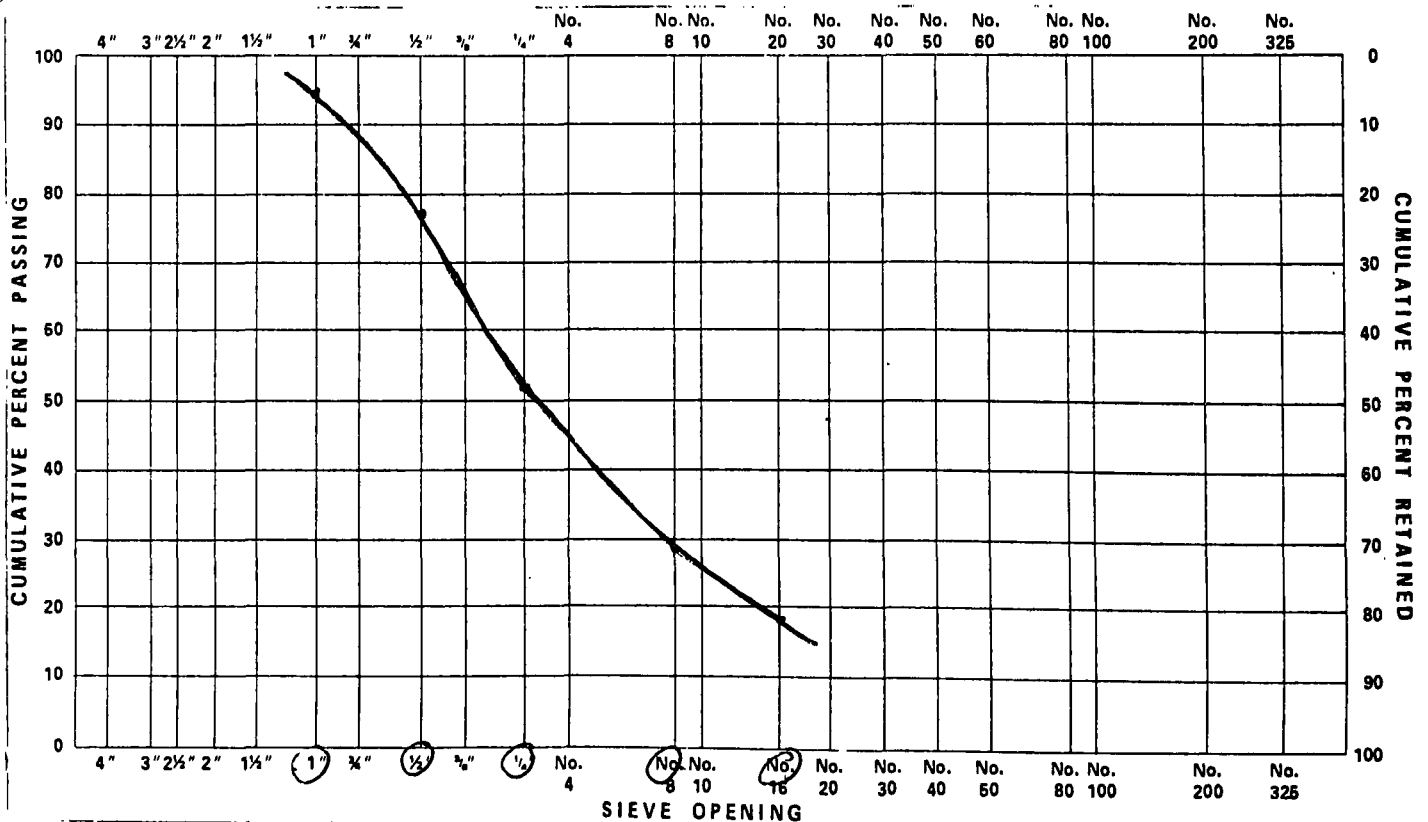
DATE SAMPLE TAKEN 10-13-77

TEST SITE A

TEST PERFORMED BY JRB

SAMPLE IDENTIFICATION KEMMERER COAL

Screen Size Passing	Tare Weight (gm)	Gross Weight (gm)	Net Weight (gm)	Percent (%)	Cumulative Weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
Top	168.9	528.4	359.5	4.93	7294.5	100.00	1
1"	168.9	1478.0	1309.1	17.95	6935.0	95.07	2
1/2"	168.9	1993.9	1825.0	25.02	5625.9	77.12	4
3/4"	168.9	1897.3	1728.4	23.69	3800.9	52.10	8
#8	168.9	967.6	798.7	10.95	2072.5	28.41	16
#16	168.9	1442.7	1273.8	17.46	1273.8	17.46	16



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. 32

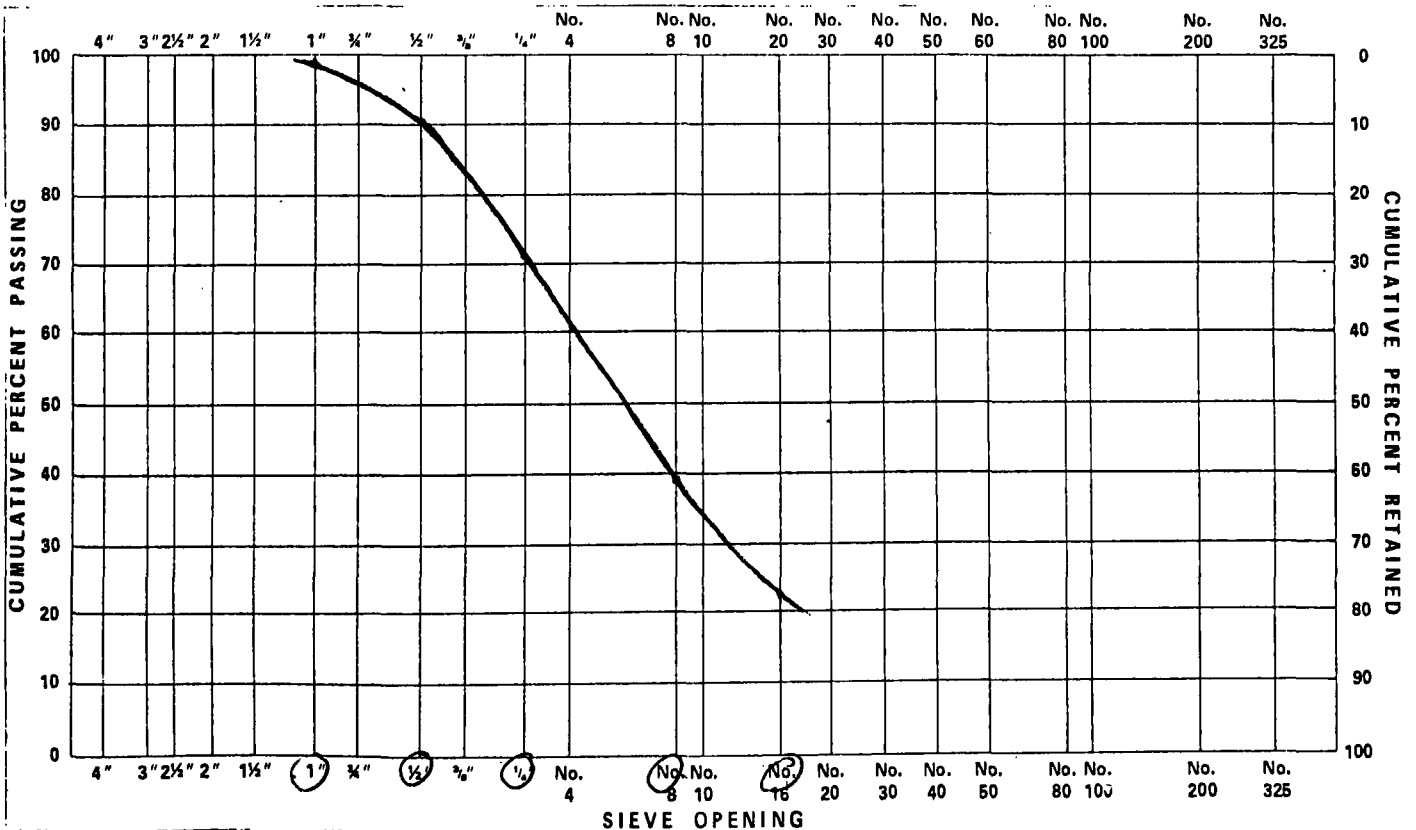
DATE SAMPLE TAKEN 15 Oct 77

TEST SITE A

TEST PERFORMED BY PSB

SAMPLE IDENTIFICATION KEMMERER COAL

Screen Size Passing	Tare Weight (gm)	Gross Weight (gm)	Net Weight (gm)	Percent (%)	Cumulative Weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
TOP	168.8	184.6 281.8	128.8	1.48	8708.2	900.00	1
1"	168.8	528.5 506.1	897.0	8.00	8579.4	98.52	2
1/2"	168.8	1002.0 981.8	1646.2	18.90	7882.4	90.52	4
1/4"	168.8	1628.1 1600.4	2890.9	33.20	6236.2	71.62	8
# 8	168.8	850.3 812.4	1325.1	15.22	3345.3	38.42	16
# 16	168.8	1202.1 1155.7	2020.2	23.20	2020.2	23.20	



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. 34

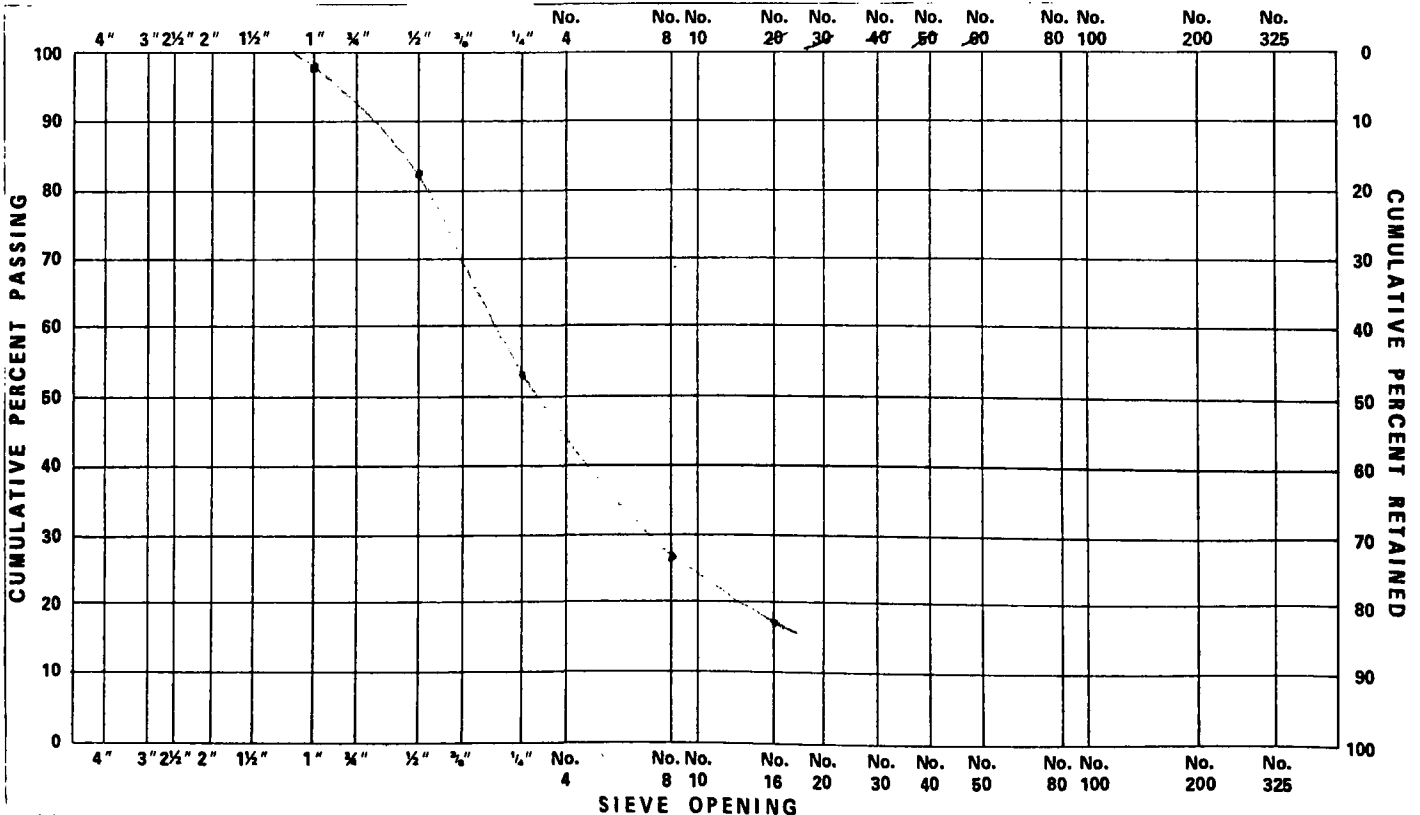
DATE SAMPLE TAKEN 10-29-77

TEST SITE A

TEST PERFORMED BY ---

SAMPLE IDENTIFICATION CONSOLIDATION COAL

Screen Size Passing	Tare Weight (gm)	Gross Weight (gm)	Net Weight (gm)	Percent (%)	Cumulative Weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
104	169.0	207.6 319.6	189.2	1.24	10,260.8	100.00	1
1"	169.0	620.6 1361.8	1650.4	16.08	10,071.6	98.16	2
1/2"	169.0	1032.6 2252.7	2947.3	28.72	8,421.2	82.08	4
3/4"	169.0	1118.4 1895.7	2676.1	26.08	5,473.9	53.36	8
#8	1690	523.5 893.8	1081.3	10.54	2,797.8	27.28	16
#16	1690	705.7 1348.8	1716.5	16.73	1,716.5	16.74	16



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. 35

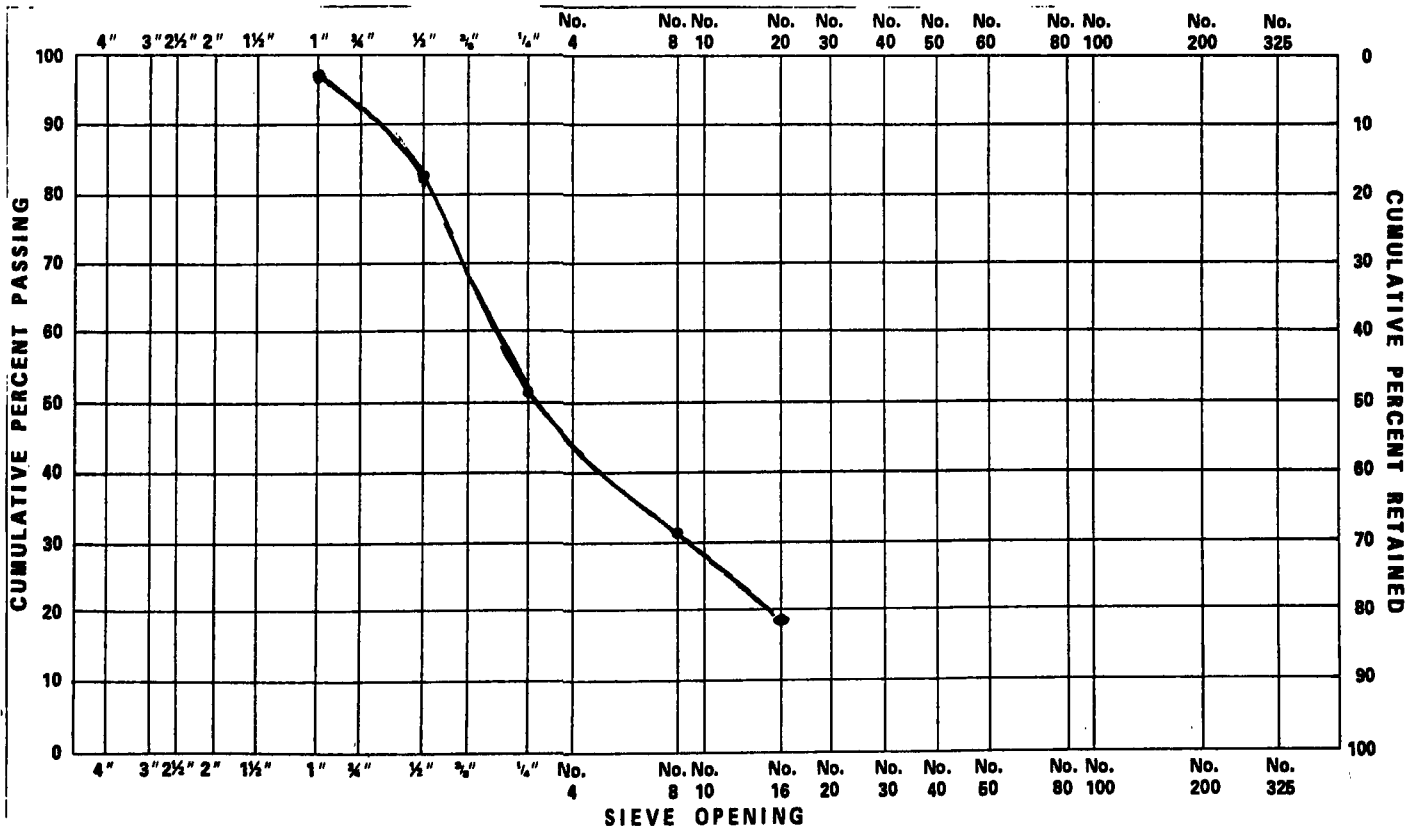
DATE SAMPLE TAKEN 10-30-77

TEST SITE A

TEST PERFORMED BY ✓ 02

SAMPLE IDENTIFICATION CONSOLIDATION CANL

Screen Size Passing	Tare Weight (gm)	Gross Weight (gm)	Net Weight (gm)	Percent (%)	Cumulative Weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
Top	169.0	351.9	182.9	2.3	7954.7	100.0	1
1"	169.0	1382.8	1213.8	15.3	7771.8	97.7	2
1/2"	169.0	966.4 1823.4	2451.8	30.8	6558.0	82.4	4
1/4"	169.0	1768.2	1599.2	20.1	4106.2	51.6	8
#8	169.0	1145.6	976.6	12.3	2507.0	31.5	16
#16	169.0	1699.4	1530.4	19.2	1530.4	19.2	—



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. 36

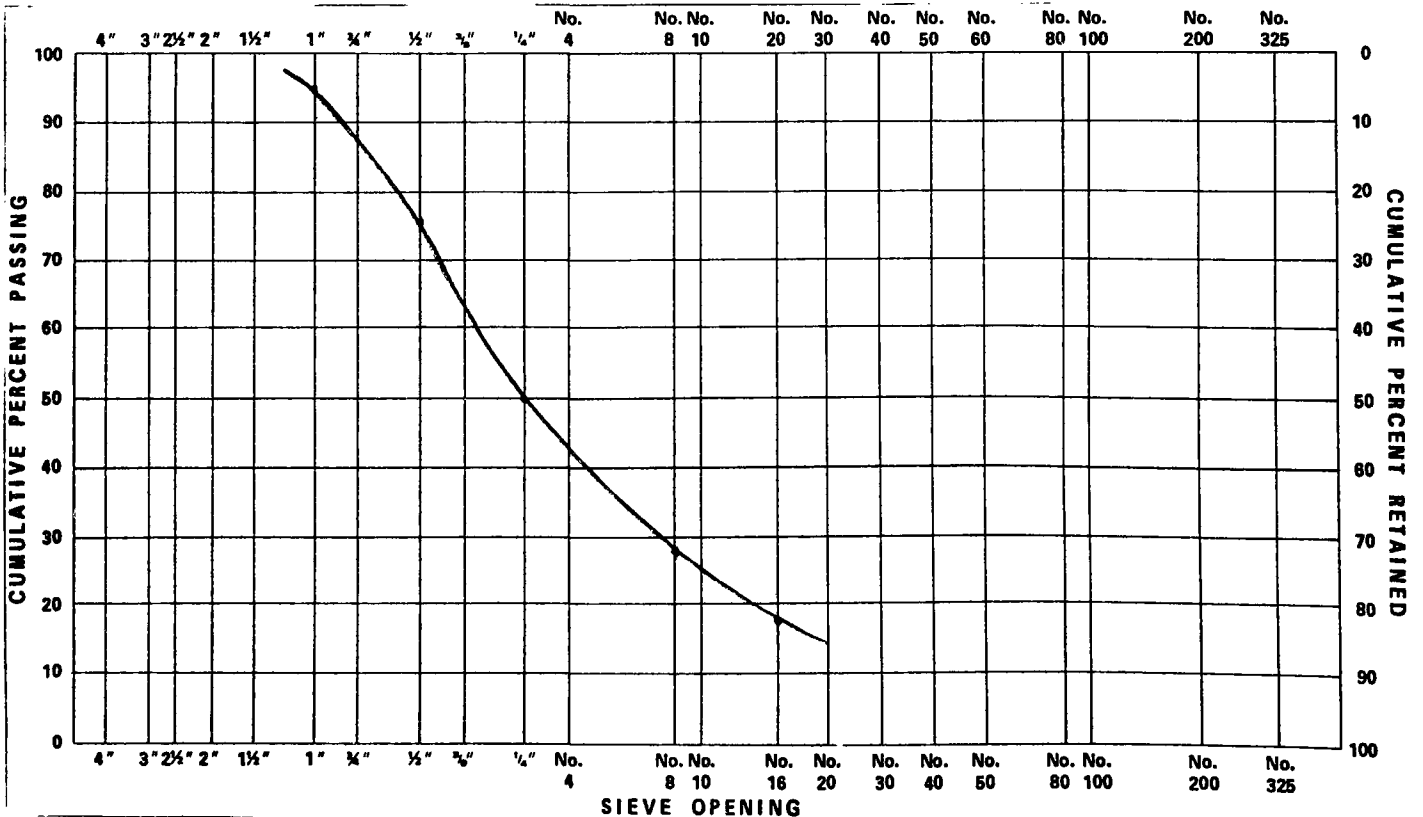
DATE SAMPLE TAKEN 11-1-77

TEST SITE A

TEST PERFORMED BY VOB

SAMPLE IDENTIFICATION CONSOLIDATION COAL

Screen Size Passing	Tare Weight (gm)	Gross Weight (gm)	Net Weight (gm)	Percent (%)	Cumulative Weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
Top	169.0	455.9	286.9	4.90	5849.4	100.00	1
1"	169.0	1345.7	1176.7	20.12	5562.5	95.10	2
1/2"	169.0	1646.8	1477.8	25.26	4385.8	74.98	4
1/4"	169.0	1491.6	1322.6	22.61	2908.0	49.72	8
#8	169.0	764.4	595.4	10.18	1585.4	27.11	16
#16	169.0	1159.0	990.0	16.92	990.0	16.93	16



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. 47

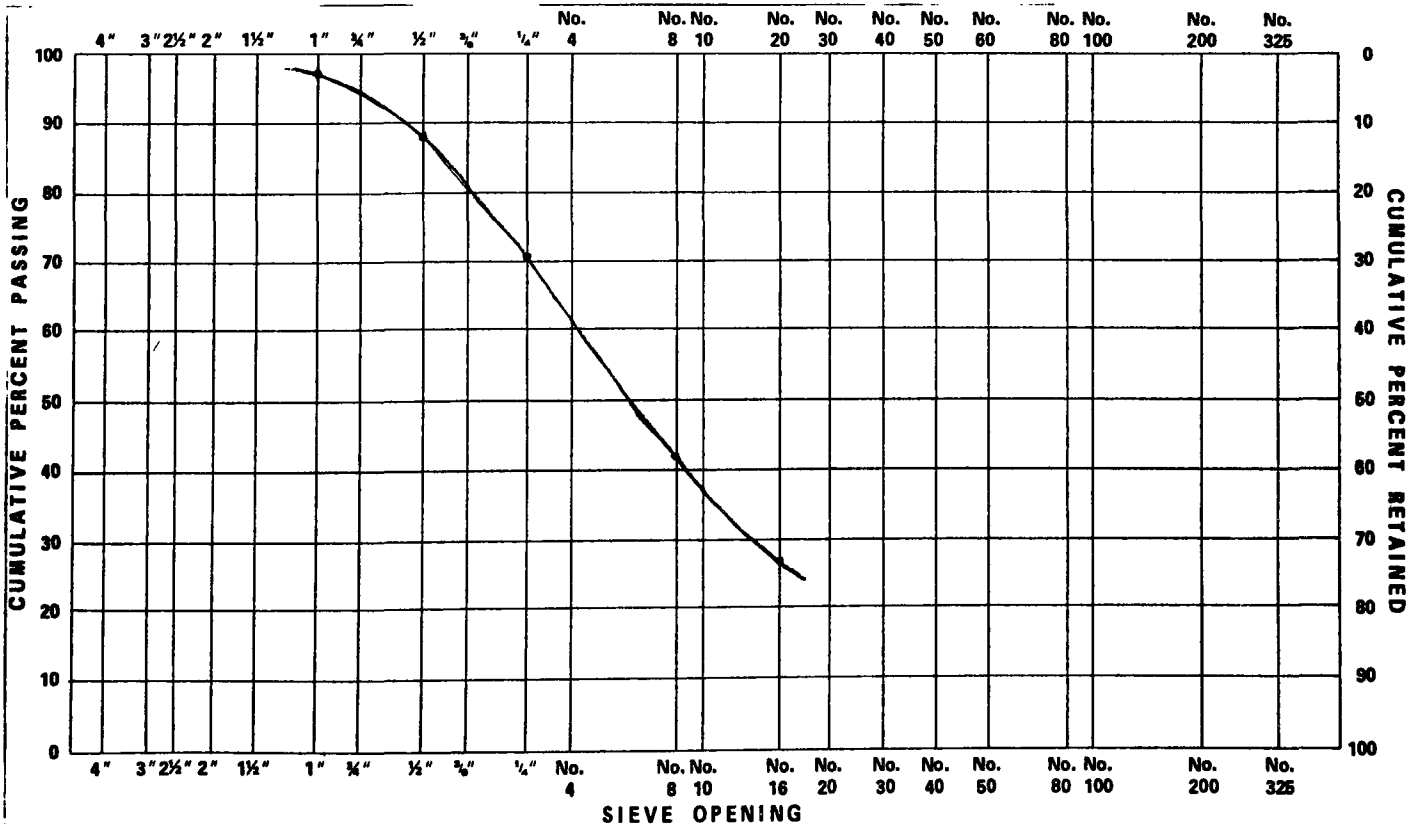
DATE SAMPLE TAKEN 11-1-77

TEST SITE A

TEST PERFORMED BY JOB

SAMPLE IDENTIFICATION CONSOLIDATION COAL

Screen Size Passing	Tare Weight (gm)	Gross Weight (gm)	Net Weight (gm)	Percent (%)	Cumulative Weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
Top	169.0	329.2	160.2	3.02	5305.0	100.00	1
1"	169.0	632.8	463.8	8.74	5144.8	96.99	2
3/4"	169.0	1130.0	961.0	18.11	4681.0	88.24	4
3/8"	169.0	1672.8	1503.8	28.35	3720.0	70.13	8
#8	169.0	977.9	808.9	15.25	2216.2	41.78	16
#16	169.0	1576.3	1407.3	26.53	1407.3	26.53	16



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. 38

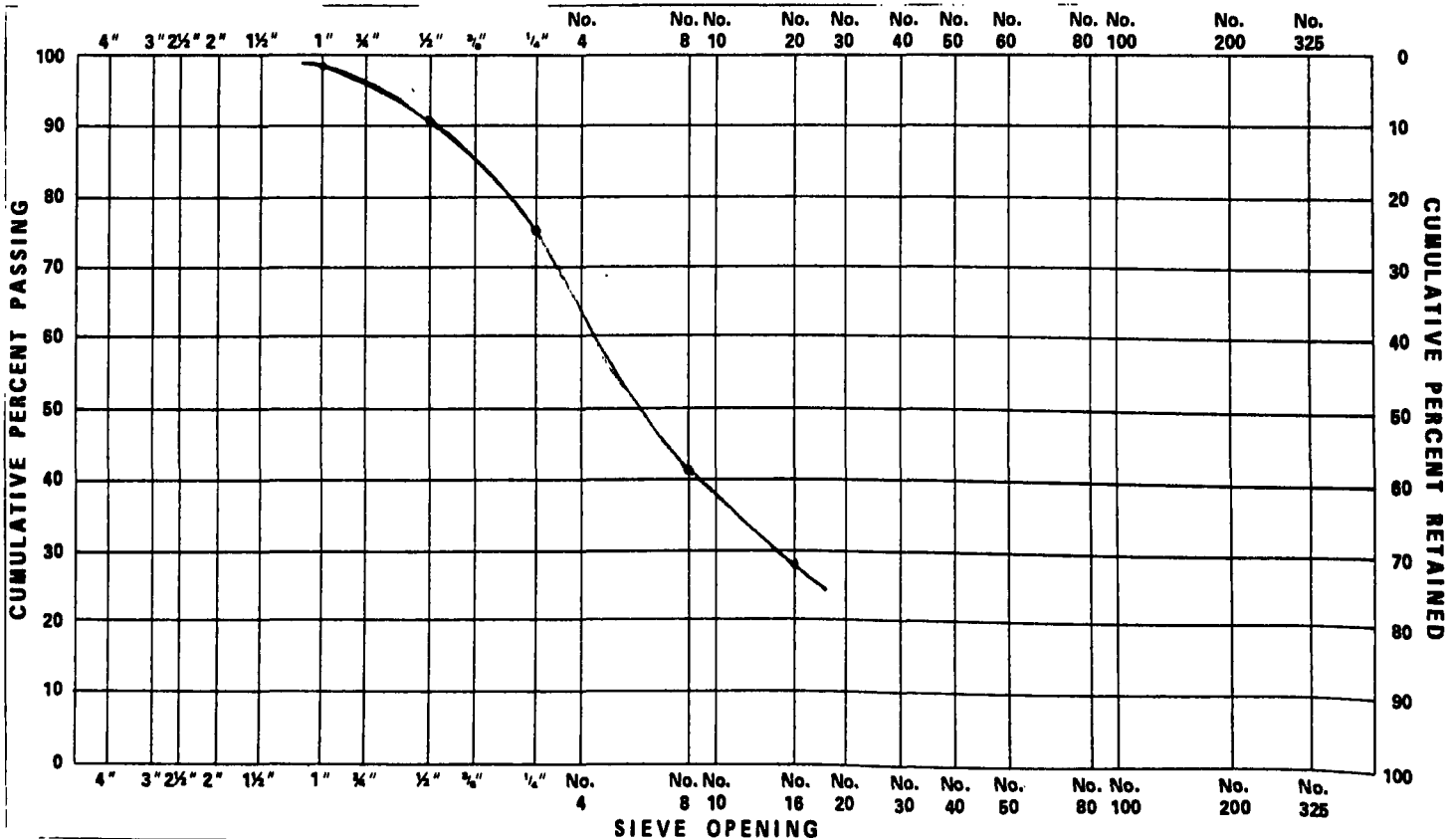
DATE SAMPLE TAKEN 11-2-77

TEST SITE A

TEST PERFORMED BY JOE

SAMPLE IDENTIFICATION CONSOLIDATION COAL

Screen Size Passing	Tare Weight (gm)	Gross Weight (gm)	Net Weight (gm)	Percent (%)	Cumulative Weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
Top	169.0	268.2	99.2	1.81	5479.0	100.00	
1"	169.0	595.2	426.2	7.78	5379.8	98.19	2
2"	169.0	1019.7	880.7	16.27	4953.6	90.41	4
4"	169.0	1993.8	1824.8	33.31	4072.9	74.34	8
#8	169.0	1139.2	715.6	13.06	2248.1	41.03	16
#16	169.0	1701.5	1532.5	27.97	1532.5	27.97	16



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. 39

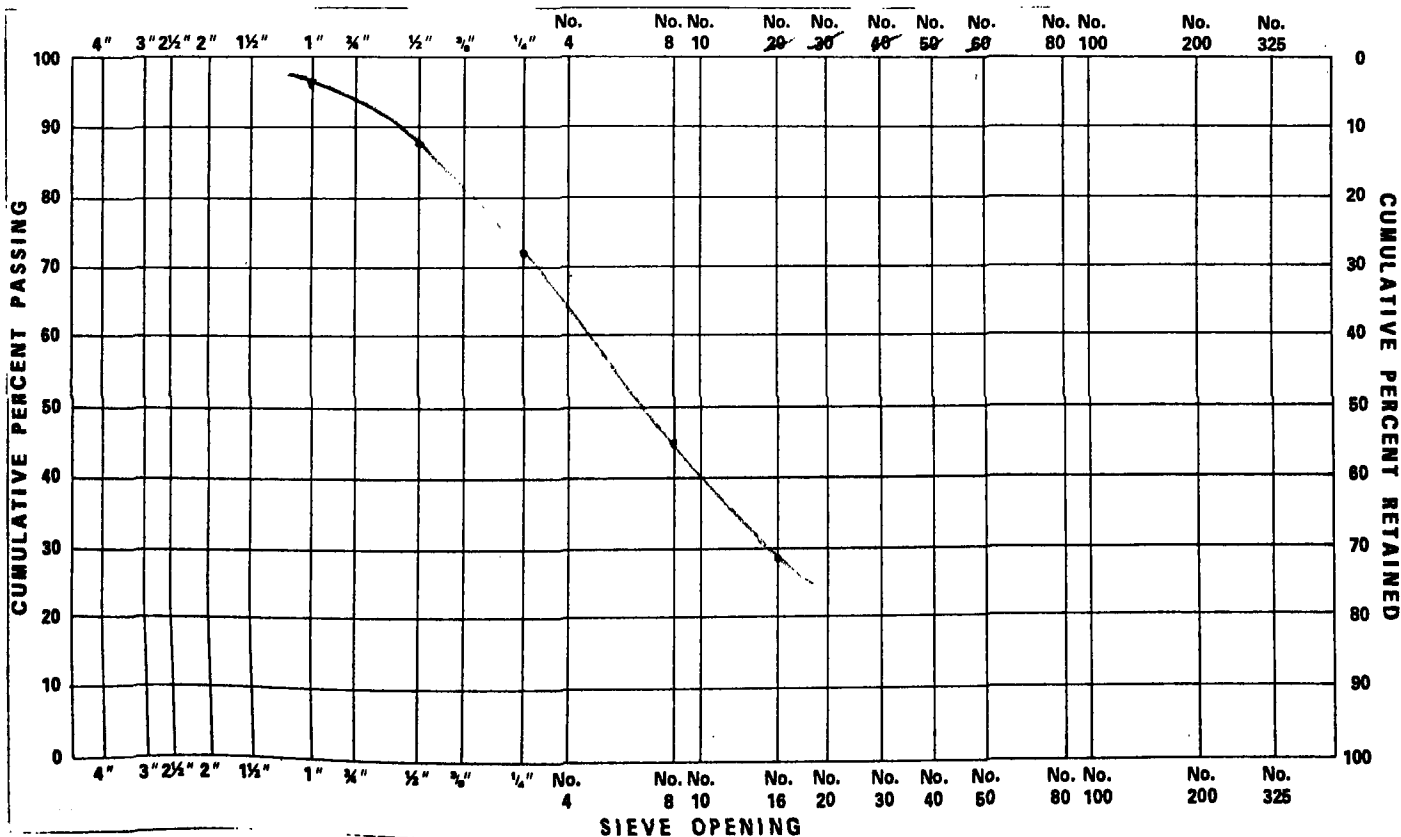
DATE SAMPLE TAKEN 11-2-77

TEST SITE A

TEST PERFORMED BY LOB

SAMPLE IDENTIFICATION CONSOLIDATION CORAL

Screen Size Passing	Tare Weight (gm)	Gross Weight (gm)	Net Weight (gm)	Percent (%)	Cumulative Weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
Top	169.0	4035	234.5	3.48	6731.9	100.00	1
1"	169.0	782.8	613.8	9.2	6497.4	96.52	2
1/2"	169.0	1197.1	1028.1	15.27	5885.5	87.40	4
1/4"	169.0	2038.3	1869.3	27.77	4855.5	72.13	8
#8	169.0	1246.1	1077.1	16.30	2986.2	44.36	16
#16	169.0	2058.1	1889.1	28.06	1889.1	28.06	16



KVB

SIEVE ANALYSIS TEST REPORT

TEST NO. 40

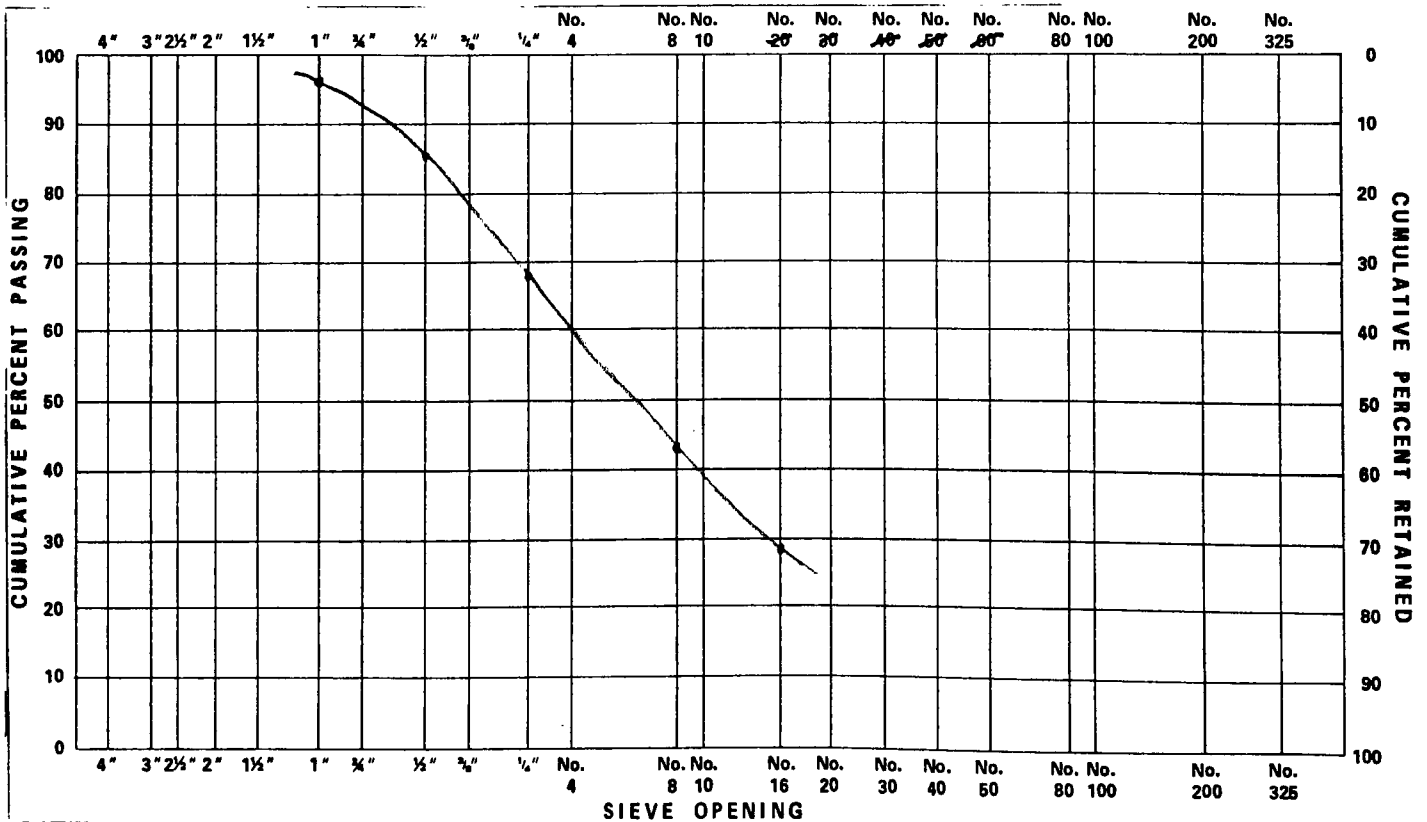
DATE SAMPLE TAKEN 11-11-77

TEST SITE A

TEST PERFORMED BY JOBS

SAMPLE IDENTIFICATION KEMMERER

Screen Size Passing	Tare Weight (gm)	Gross Weight (gm)	Net Weight (gm)	Percent (%)	Cumulative Weight Passing (gm)	Cumulative Percent Passing (%)	Sieve Shaker Duration (min)
TOP	168.7	507.6	338.9	3.50	9673.7	100.00	1
1"	168.7	1176.5	1007.8	10.42	9334.8	96.50	2
1/2"	168.7	1916.1	1747.4	18.06	8327.0	86.08	4
1/4"	168.7	2582.1	2413.4	24.95	6579.6	68.02	8
#8	168.7	1579.8	1411.1	14.59	4166.2	43.07	16
#16	168.7	2065.9 1026.6	2755.1	28.48	2755.1	28.48	16



TECHNICAL REPORT DATA <i>(Please read Instructions on the reverse before completing)</i>			
1. REPORT NO. EPA-600/7-78-136b		3. RECIPIENT'S ACCESSION NO.	
4. TITLE AND SUBTITLE Field Tests of Industrial Stoker Coal-fired Boilers for Emissions Control and Efficiency Improvement--Site A (Data Supplement)		5. REPORT DATE December 1978	
7. AUTHOR(S) J.E. Gabrielson, P.L. Langsjoen, and T.C. Kosvic		6. PERFORMING ORGANIZATION CODE	
9. PERFORMING ORGANIZATION NAME AND ADDRESS KVB, Inc. 6176 Olson Memorial Highway Minneapolis, Minnesota 55422		8. PERFORMING ORGANIZATION REPORT NO.	
12. SPONSORING AGENCY NAME AND ADDRESS EPA, Office of Research and Development * Industrial Environmental Research Laboratory Research Triangle Park, NC 27711		10. PROGRAM ELEMENT NO. EHE624	
		11. CONTRACT/GRANT NO. EPA-IAG-D7-E681 and DOE-EF-77-C-01-2609	
		13. TYPE OF REPORT AND PERIOD COVERED Supplement; 6-12/77	
		14. SPONSORING AGENCY CODE EPA/600/13 and DoE	
15. SUPPLEMENTARY NOTES IERL-RTP project officer is R.E. Hall. (*) Cosponsors are DoE (W.T. Harvey, Jr.) and the American Boiler Manufacturers Association.			
16. ABSTRACT The supplement is a compilation of test data in greater detail than was practical in the final report. It provides details to other researchers who are interested in performing their own analysis. Readers are referred to the final report for: objectives; descriptions of the facility tested, coals fired, test equipment, and procedures; interpretations; and conclusions. The final report also contains data summaries not found in the supplement. The supplement contains panel board data for each test; detailed particulate, O₂, CO₂, CO, NO, SO₂, and SO₃ data; particle size distribution data; modified spoke spot data; and data on chemical analysis of the coal and coal size consistency.			
17. KEY WORDS AND DOCUMENT ANALYSIS			
a. DESCRIPTORS		b. IDENTIFIERS/OPEN ENDED TERMS	c. COSATI Field/Group
Air Pollution	Improvement	Air Pollution Control	13B
Boilers	Efficiency	Stationary Sources	13A
Combustion	Flue Gases	Combustion Modification	21B
Coal	Fly Ash	Spreader Stokers	21D
Field Tests	Particle Size	Particulate	14B
Dust	Nitrogen Oxides	Overfire Air	11G
Stokers	Sulfur Oxides	Flyash Reinjection	07B
18. DISTRIBUTION STATEMENT Unlimited		19. SECURITY CLASS (This Report) Unclassified	21. NO. OF PAGES 278
		20. SECURITY CLASS (This page) Unclassified	22. PRICE