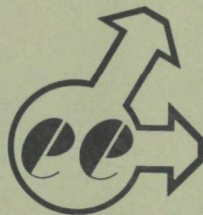


TEST NO. 71 - CI - 37
C. F. CHEMICALS, INC.
DIAMMONIUM PHOSPHATE
BARTOW, FLORIDA
DECEMBER 16 - 20, 1971



environmental engineering, inc.

2324 S. W. 34th STREET / GAINESVILLE, FLORIDA 32601 / PHONE 904 / 372-3318

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Tests Conducted by:
ENVIRONMENTAL ENGINEERING, INC.
Contract # CPA - 70 - 82

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INTRODUCTION

Under the direction of the Environmental Protection Agency, Environmental Engineering, Inc. conducted emission tests at the C. F. Chemicals, Inc. diammonium phosphate plant number three located in Bartow, Florida. Three test runs were conducted on December 16 - 20, 1971. The purpose of the tests was to obtain data for the use of both the Industrial Studies Branch and the Performance Standards Branch of the EPA.

Using separate sample trains, measurements were made for both total fluorides and ammonia in the inlet and outlet ducts of the reactor, cooler, and dryer scrubbers. Grab samples of the scrubbing liquids, the process reactants, and the process products were taken and analyzed for fluoride and P_2O_5 content. A schematic flow diagram of all the sampling locations is given in Figure I.

Pertinent results of the tests are listed in Tables I - XII; complete test results are given in Appendix A.

SUMMARY OF RESULTS

The plant operated under normal process conditions during the three test runs. However, two minor irregularities occurred in the sampling. During the third run at Station "L", the probe became plugged with solid material and the nozzle had to be removed and cleaned before the test could be continued. Secondly, at Station "M", negative flow occurred at the first three traverse points and these points were therefore skipped during the sample runs. In determining total stack gas flow rates, a value of zero velocity was used for these negative points.

A few irregularities in the test data need to be noted. For run number two the total fluoride concentration measured at the reactor scrubber outlet is greater than the fluoride concentration at the inlet (see Tables I and VI). Like wise, for both runs number two and three the ammonia concentrations measured at the cooler scrubber outlet are higher than the concentrations at the scrubber inlet (see Tables X and

XI). With the exception that perhaps some of these samples were contaminated, no explanation for these anomalies has been confirmed. For a complete summary of the stack conditions and emission levels for each test run refer to Tables I - XII.

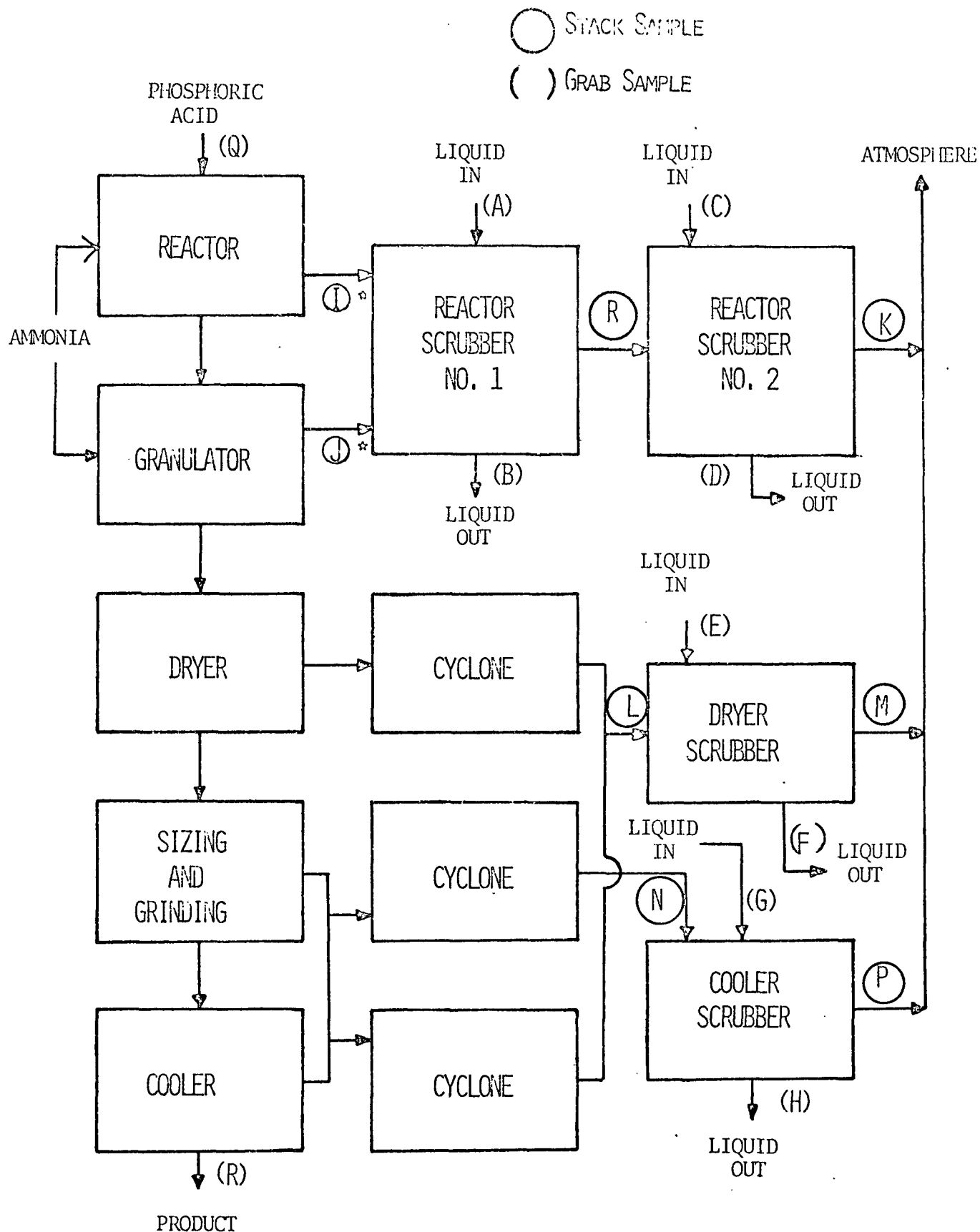


FIGURE 1

SCHEMATIC LOCATIONS OF SAMPLING STATIONS,
DIAMMONIUM PHOSPHATE PLANT NO. 3, C. F. CHEMICALS, INC.

* These points could not be sampled because of plugging problems.

TABLE 1
SUMMARY OF RESULTS
FLUORIDES
STATION "K" SECOND STAGE
REACTOR SCRUBBER OUTLET

Run No.	1	2	3
Date	12-16-71	12-18-71	12-20-71
Barometric pressure, inches Hg	30	30	30
Stack pressure, inches Hg	29	29	29
Stack gas moisture, % volume	22.6	27	23.6
Average stack gas temperature, °F.	164	169	170
Stack gas flow rate @ S.T.P., SCFH	23066	33660	21940
Vol. dry gas @ S.T.P. *, SCF	104.233	133.2	102.895
Fluoride, water soluble, mg	67	147	57
Fluoride, total, mg	67.67	147.77	64.3
Fluoride, water soluble, gr/SCF	0.0095	0.0169	0.0084
Fluoride, total, gr/SCF	0.0096	0.017	0.0095
Fluoride, water soluble, gr/CF stk. cond.	0.0061	0.0101	0.0052
Fluoride, total, gr/CF stk. cond.	0.0061	0.0101	0.0059
Fluoride, water soluble, lb/hour	1.88	4.87	1.58
Fluoride, total, lb/hour	1.90	4.90	1.78
Fluoride, water soluble, lb/ton P_2O_5 Fed.	0.06	0.19	0.06
Fluoride, total, lb/ton P_2O_5 Fed.	0.07	0.20	0.07
Second Stage Scrubber Efficiency, %	44.3	----	82.3

* Dry, 70°F., 29.92 inches Hg.

TABLE 2

SUMMARY OF RESULTS
FLUORIDES
STATION "L" DRYER
SCRUBBER INLET

Run No.	1	2	3
Date	12-16-71	12-18-71	12-20-71
Barometric pressure, inches Hg	30	30	30
Stack pressure, inches Hg	30	30	30
Stack gas moisture, % volume	19.5	10.4	9
Average stack gas temperature, °F.	160	150	151
Stack gas flow rate @ S.T.P., SCFM	30655	36625	34855
Vol. dry gas @ S.T.P. *, SCF	85.228	88.388	81.827
Fluoride, water soluble, mg	154	91	22.6
Fluoride, total, mg	216	141	37.9
Fluoride, water soluble, gr/SCF	0.0252	0.0149	0.004
Fluoride, total, gr/SCF	0.0354	0.0231	0.0066
Fluoride, water soluble, gr/CF stk. cond.	0.0174	0.0116	0.0031
Fluoride, total, gr/CF stk. cond.	0.0244	0.018	0.0052
Fluoride, water soluble, lb/hour	6.62	4.68	1.18
Fluoride, total, lb/hour	9.29	7.25	1.98
Fluoride, water soluble, lb/ton P_2O_5 Fed.	0.23	0.19	0.05
Fluoride, total, lb/ton P_2O_5 Fed.	0.32	0.29	0.08
Scrubber efficiency, %	----	----	----

* Dry, 70°F., 29.92 inches Hg.

TABLE 3
SUMMARY OF RESULTS
FLUORIDES
STATION "M" DRYER
SCRUBBER OUTLET

Run No.	1	2	3
Date	12-16-71	12-18-71	12-20-71
Barometric pressure, inches Hg	30	30	30
Stack pressure, inches Hg	28.1	28.1	28.2
Stack gas moisture, % volume	11.7	11.7	14.3
Average stack gas temperature, °F.	132	111	111
Stack gas flow rate @ S.T.P., SCFM	39130	36103	31979
Vol. dry gas @ S.T.P.* , SCF	80.528	80.301	79.294
Fluoride, water soluble, mg	2.4	8.1	1.2
Fluoride, total, mg	2.466	8.42	1.41
Fluoride, water soluble, gr/SCF	0.0004	0.0015	0.0002
Fluoride, total, gr/SCF	0.0005	0.0016	0.0003
Fluoride, water soluble, gr/CF stk. cond.	0.0003	0.0012	0.0002
Fluoride, total, gr/CF stk. cond.	0.0003	0.0012	0.0002
Fluoride, water soluble, lb/hour	0.15	0.48	0.07
Fluoride, total, lb/hour	0.15	0.51	0.08
Fluoride, water soluble, lb/ton P_2O_5 Fed.	0.005	0.019	0.003
Fluoride, total, lb/ton P_2O_5 Fed.	0.005	0.020	0.003
Scrubber efficiency, %	98.4	93.0	96.0

* Dry, 70°F., 29.92 inches Hg.

TABLE 4
SUMMARY OF RESULTS
FLUORIDES
Station "N" Cooler
Scrubber Inlet

Run No.	1	2	3
Date	12-16-71	12-18-71	12-20-71
Barometric pressure, inches Hg	30.	30	30
Stack pressure, inches Hg	29.71	29.71	29.71
Stack gas moisture, % volume	2.6	2.1	2.5
Average stack gas temperature, °F.	121	121	121
Stack gas flow rate @ S.T.P., SCFM	36019	34373	41447
Vol. dry gas @ S.T.P. *, SCF	75.538	74.057	84.862
Fluoride, water soluble, mg	34	25	31
Fluoride, total, mg	64.2	43.5	48.6
Fluoride, water soluble, gr/SCF	0.0065	0.0052	0.0055
Fluoride, total, gr/SCF	0.0123	0.009	0.0086
Fluoride, water soluble, gr/CF stk. cond.	0.0055	0.0044	0.0047
Fluoride, total, gr/CF stk. cond.	0.0105	0.0077	0.0074
Fluoride, water soluble, lb/hour	2.00	1.52	1.96
Fluoride, total, lb/hour	3.74	2.65	3.07
Fluoride, water soluble, lb/ton P_2O_5 Fed.	0.07	0.06	0.08
Fluoride, total, lb/ton P_2O_5 Fed.	0.13	0.11	0.12
Scrubber efficiency, %			

* Dry, 70°F., 29.92 inches Hg.

TABLE 5
SUMMARY OF RESULTS
FLUORIDES
STATION "P" COOLER
SCRUBBER OUTLET

Run No.	1	2	3
Date	12-16-71	12-18-71	12-20-71
Barometric pressure, inches Hg	30	30	30
Stack pressure, inches Hg	28.7	28.7	28.7
Stack gas moisture, % volume	11.4	9.5	7.5
Average stack gas temperature, °F.	124	100	95
Stack gas flow rate @ S.T.P., SCFM	46921	52423	60675
Vol. dry gas @ S.T.P. *, SCF	83.789	99.759	114.24
Fluoride, water soluble, mg	2.8	4.6	2.7
Fluoride, total, mg	2.8	4.671	2.751
Fluoride, water soluble, gr/SCF	0.0005	0.0007	0.0003
Fluoride, total, gr/SCF	0.0005	0.0007	0.0003
Fluoride, water soluble, gr/CF stk. cond.	0.0004	0.0006	0.0003
Fluoride, total, gr/CF stk. cond.	0.0004	0.0006	0.0003
Fluoride, water soluble, lb/hour	0.19	0.30	0.18
Fluoride, total, lb/hour	0.19	0.31	0.18
Fluoride, water soluble, lb/ton P_2O_5 Fed.	0.007	0.012	0.007
Fluoride, total, lb/ton P_2O_5 Fed.	0.007	0.012	0.007
Scrubber efficiency, %	95.0	88.3	94.1

* Dry, 70°F., 29.92 inches Hg.

TABLE 6
SUMMARY OF RESULTS
FLUORIDES
STATION " R" SECOND STAGE
REACTOR SCRUBBER INLET

Run No.	1	2	3
Date	12-16-71	12-18-71	12-20-71
Barometric pressure, inches Hg	30	30	30
Stack pressure, inches Hg	29	29	29
Stack gas moisture, % volume	29	30.2	32.5
Average stack gas temperature, °F.	171	171	173
Stack gas flow rate @ S.T.P., SCFM	19812	19019	17540
Vol. dry gas @ S.T.P.* , SCF	120.332	91.427	84.318
Fluoride, water soluble, mg	143	71	319
Fluoride, total, mg	164.4	91.3	373
Fluoride, water soluble, gr/SCF	0.0175	0.012	0.0571
Fluoride, total, gr/SCF	0.0201	0.0154	0.0667
Fluoride, water soluble, gr/CF stk. cond.	0.0101	0.0068	0.0312
Fluoride, total, gr/CF stk. cond.	0.0116	0.0088	0.0365
Fluoride, water soluble, lb/hour	2.96	1.96	8.58
Fluoride, total, lb/hour	3.41	2.51	10.03
Fluoride, water soluble, lb/ton P_2O_5 Fed.	0.10	0.08	0.34
Fluoride, total, lb/ton P_2O_5 Fed.	0.12	0.10	0.40
Scrubber efficiency, %	----	----	----

* Dry, 70°F., 29.92 inches Hg.

TABLE 7
SUMMARY OF RESULTS
AMMONIA
STATION "K" SECOND STAGE
Reactor Scrubber Outlet

Run No.	1	2	3
Date	12-16-71	12-18-71	12-20-71
Barometric pressure, inches Hg	30	30	30
Stack pressure, inches Hg	29	29	29
Stack gas moisture, % volume	22.6	27	23.6
Average stack gas temperature, °F.	164	170	170
Stack gas flow rate @ S.T.P. SCFM.	23066	33660	21940
Vol. dry gas @ S.T.P. *, SCF	3.133	3.033	2.854
Ammonia, mg	1.3	1.8	0.3
Ammonia, gr/SCF	0.006	0.009	0.002
Ammonia, gr/CF	0.004	0.005	0.001
Ammonia, lbs/hour	1.26	2.64	0.30
Ammonia lb/ton NH ₃ fed	0.27	0.24	0.03
Scrubber efficiency - %, Second Stage	97.6	99.7	99.9

* Dry, 70°F., 29.92 inches Hg.

TABLE 8
SUMMARY OF RESULTS
AMMONIA
STATION "L"
Dryer Scrubber Inlet

Run No.	1	2	3
Date	12-16-71	12-18-71	12-20-71
Barometric pressure, inches Hg	30	30	30
Stack pressure, inches Hg	29.7	29.7	29.7
Stack gas moisture, % volume	19.5	10.4	9
Average stack gas temperature, °F.	160	150	151
Stack gas flow rate @ S.T.P. SCFM.	30655	36625	34855
Vol. dry gas @ S.T.P. *, SCF	2.731	2.826	2.758
Ammonia, mg	170.5	126.7	160.3
Ammonia, gr/SCF	0.96	0.69	0.89
Ammonia, gr/CF	0.65	0.53	0.70
Ammonia, lbs/hour	252.6	216.7	267.4
Ammonia lb/ton NH ₃ fed	54.9	19.3	25.7
Scrubber efficiency - %	----	----	----

* Dry, 70°F., 29.92 inches Hg.

TABLE 9
SUMMARY OF RESULTS
AMMONIA
STATION 'M'
Dryer Scrubrr Outlet

Run No.	1	2	3
Date	12-16-71	12-18-71	12-20-71
Barometric pressure, inches Hg	30	30	30
Stack pressure, inches Hg	28.1	28.1	28.1
Stack gas moisture, % volume	11.7	11.7	14.3
Average stack gas temperature, °F.	132	111	111
Stack gas flow rate @ S.T.P. SCFM.	39130	36103	31979
Vol. dry gas @ S.T.P.* , SCF	3.049	3.103	2.950
Ammonia, mg	0.04	2	1
Ammonia, gr/SCF	0.0002	0.0099	0.0052
Ammonia, gr/CF	0.0001	0.0076	0.0039
Ammonia, lbs/hour	0.07	3.07	1.43
Ammonia lb/ton NH ₃ fed	0.015	0.274	0.138
Scrubber efficiency - %	99.9	98.6	99.5

* Dry, 70°F., 29.92 inches Hg.

TABLE 10
SUMMARY OF RESULTS
AMMONIA

STATION "N"
Cooler Scrubber Inlet

Run No.	1	2	3
Date	12-16-71	12-18-71	12-20-71
Barometric pressure, inches Hg	30	30	30
Stack pressure, inches Hg	29.7	29.7	29.7
Stack gas moisture, % volume	2.6	2.1	2.5
Average stack gas temperature, °F.	140	140	140
Stack gas flow rate @ S.T.P. SCFM.	36019	34373	41447
Vol. dry gas @ S.T.P.* , SCF	2.812	3.519	3.027
Ammonia, mg	23.2	0.05	0.1
Ammonia, gr/SCF	0.13	0.0002	0.0005
Ammonia, gr/CF	0.108	0.0002	0.0004
Ammonia, lbs/hour	39.2	0.06	0.18
Ammonia lb/ton NH ₃ fed	8.5	0.006	0.017
Scrubber efficiency - %	----	----	----

* Dry, 70°F., 29.92 inches Hg.

TABLE 11
SUMMARY OF RESULTS
AMMONIA
STATION "P"
Cooler Scrubber Outlet

Run No.	1	2	3
Date	12-16-71	12-18-71	12-20-71
Barometric pressure, inches Hg	30	30	30
Stack pressure, inches Hg	28.7	28.7	28.7
Stack gas moisture, % volume	11.4	9.5	7.5
Average stack gas temperature, °F.	124	100	95
Stack gas flow rate @ S.T.P. SCFM.	46921	52423	60675
Vol. dry gas @ S.T.P. *, SCF	3.179	3.773	3.557
Ammonia, mg	1.6	1	0.2
Ammonia, gr/SCF	0.008	0.004	0.0009
Ammonia, gr/CF	0.006	0.003	0.0007
Ammonia, lbs/hour	3.1	1.8	0.4
Ammonia lb/ton NH ₃ fed	0.68	0.16	0.04
Scrubber efficiency - %	98.7	----	----

* Dry, 70°F., 29.92 inches Hg.

TABLE 12

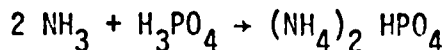
SUMMARY OF RESULTS
AMMONIASTATION "R" SECOND STAGE
Reactor Scrubber Inlet

Run No.	1	2	3
Date	12-16-71	12-18-71	12-20-71
Barometric pressure, inches Hg	30	30	30
Stack pressure, inches Hg	29	29	29
Stack gas moisture, % volume	29	30.2	32.5
Average stack gas temperature, °F.	174	171	173
Stack gas flow rate @ S.T.P. SCFM.	19812	19019	17540
Vol. dry gas @ S.T.P.* , SCF	2.857	3.443	2.667
Ammonia, mg	57.9	1267.9	257.4
Ammonia, gr/SCF	0.31	5.6	1.5
Ammonia, gr/CF	0.18	3.2	0.8
Ammonia, lbs/hour	53	924	223
	4.6	11.2	10.4
Ammonia lb/ton NH ₃ fed	11.5	82.5	21.5
Scrubber efficiency - %	----	----	----

* Dry, 70°F., 29.92 inches Hg.

PROCESS DESCRIPTION

The process consists of a preneutralizer for ammoniation of wet-process phosphoric acid, an ammoniator-granulator, and accessory equipment for drying, cooling, and screening the product. The primary reaction is as follows:



Unabsorbed ammonia gas flows out with exhaust gases; however, most of this ammonia is returned to the process by means of a scrubbing system using weak phosphoric acid as the scrubbing medium.

The scrubber acid is mixed with 54 percent P_2O_5 acid (from the wet-acid plant) in the preneutralizer resulting in a solution usually averaging about 39 percent P_2O_5 .

The DAP slurry is pumped from the reactor to the granulator where additional ammonia is added along with recycled product to form a solid material averaging 18 percent N and 46 percent P_2O_5 . Then it is dried, cooled, and screened before being conveyed to storage.

PROCESS OPERATION

Run #1 was conducted on December 16, 1971, from 4:20 to 6:20 p.m. Process operation was normal for the duration of the run. Before the start of Run #2 the next morning, the 30% P_2O_5 acid line to

the scrubbers plugged forcing the plant to switch to 54% P_2O_5 makeup acid. This change altered the strength of the scrubbing acid which constituted an abnormal condition. Testing had to be postponed until the 30% P_2O_5 line could be reopened.

At 9:35 a.m. on the morning of the 18th, the test crew had just begun Run #2 when a power failure shut the plant down. The plant started up again at 9:50 a.m.; only to shut down again at 10:30 a.m. when a slurry pump plugged. At 12:40 p.m. the unit started up again and continued to run without difficulty for the rest of the day. Run #2 was conducted under normal process conditions from 1:45 p.m. to 3:45 p.m.

Plant operating problems were also experienced on the next morning. A vibration problem with the ammoniator and screen fans caused a shutdown at 7:55 a.m. Dust buildup on the fan blades was removed by sandblasting and the plant started up again at 11:30 a.m. After the plant had been in operation a short time, the duct from the reactor to the scrubber plugged causing excessive ammonia fumes from the reactor to be leaked into the area. The plant was started up again at 5:30 p.m. High pH and decreasing specific gravities were observed on both scrubber acid sumps just prior to the start of Run #3 at 6:05 p.m. However, the plant operator indicated that this condition would be quickly stabilized. Other than some minor adjustments to the ammonia feed rate, process operation remained normal throughout Run #3 which was concluded at 8:30 p.m.

LOCATION OF SAMPLING POINTS

The sampling sites and number of traverse points were selected as per "Method I-Sampling and Velocity Traverses for Stationary Sources, Part 60, Subchapter C, Chapter 1, Title 40," Federal Register, No. 247-Pt. II-1.

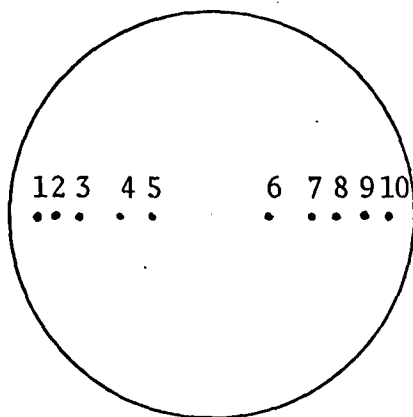
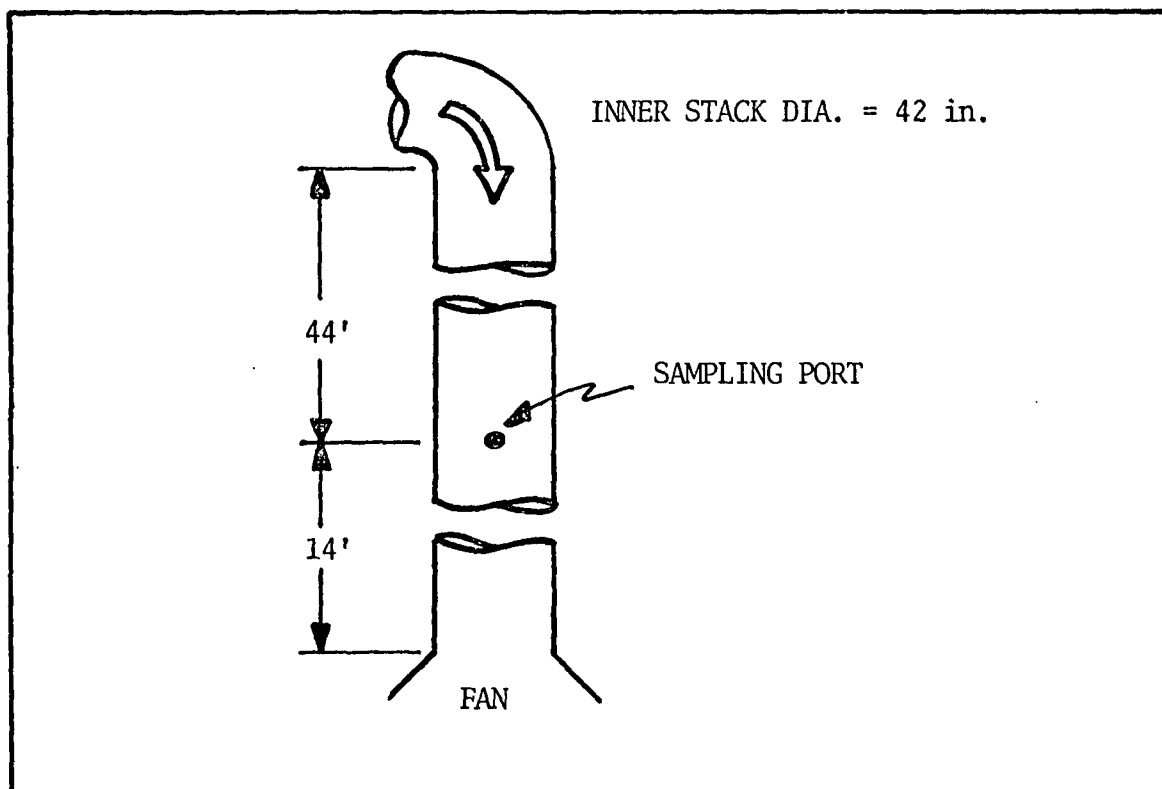
The above method suggests using two perpendicular diameters of traverse points per sampling station, however, on-site conditions necessitated the use of only one traverse diameter in all cases. The suggested number of traverse points per diameter was used where possible without sampling within one inch of the inner wall.

Figures 2 through 7 are schematic diagrams of the stack configuration near the sampling location, and the sampling points traversed during the emission tests.

TABLE 13

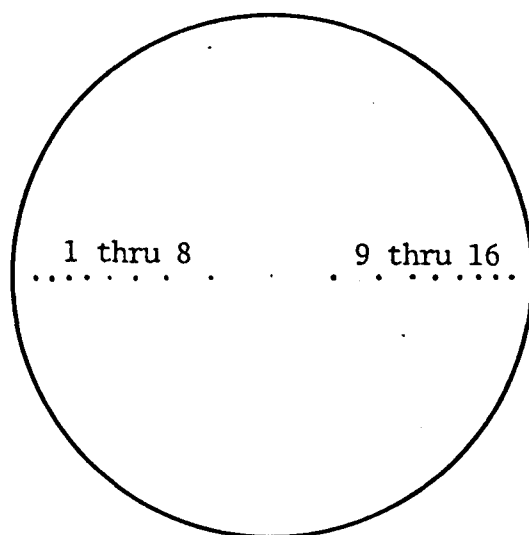
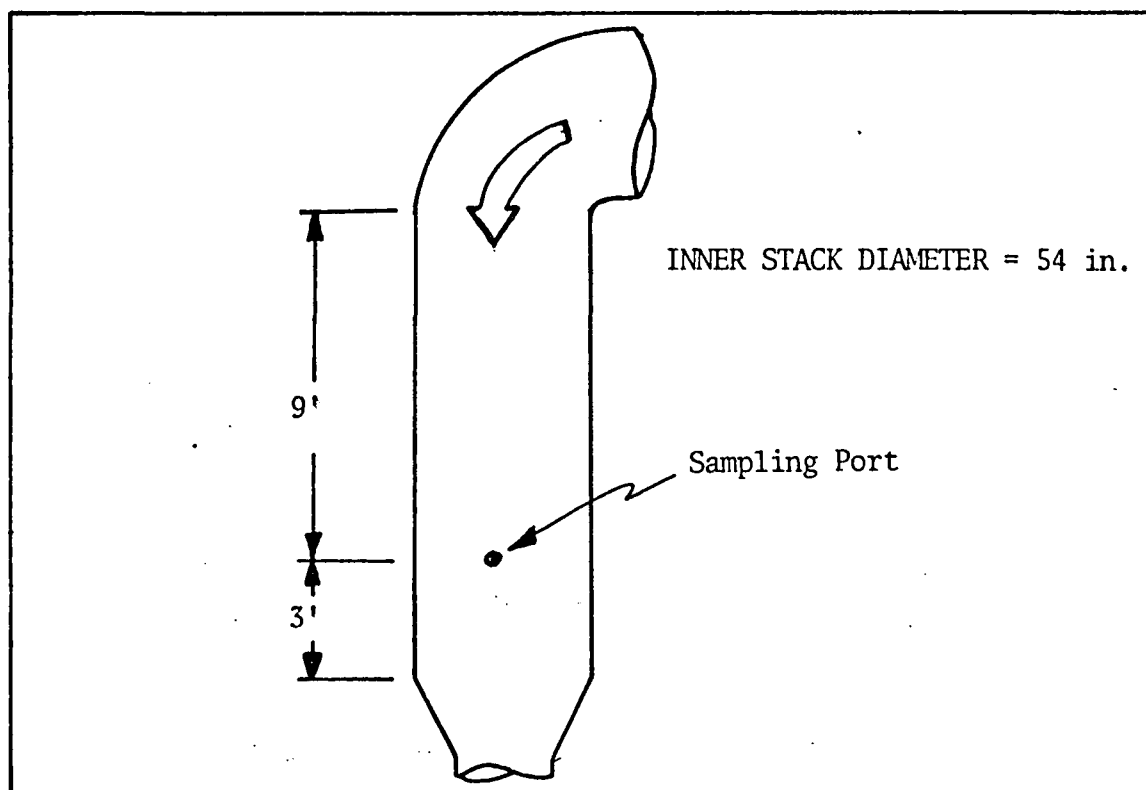
DESCRIPTION OF SAMPLING POINTS

Sampling Point Description	Sampling Point Identification	Actual Number of Traverse Points	Stack Diameter(ft.)
Reactor Scrubber Outlet	K	10	3.5
Dryer Scrubber Inlet	L	16	4.5
Dryer Scrubber Outlet	M	20	4.6
Cooler Scrubber Inlet	N	22	5.0
Cooler Scrubber Outlet	P	18	5.0
Reactor Scrubber Inlet	R	22	3.1



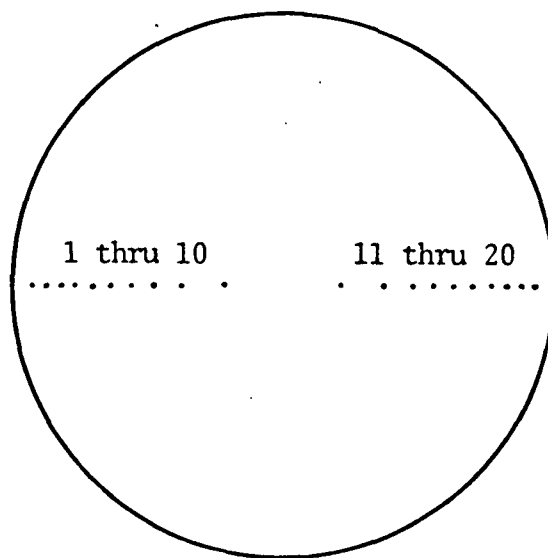
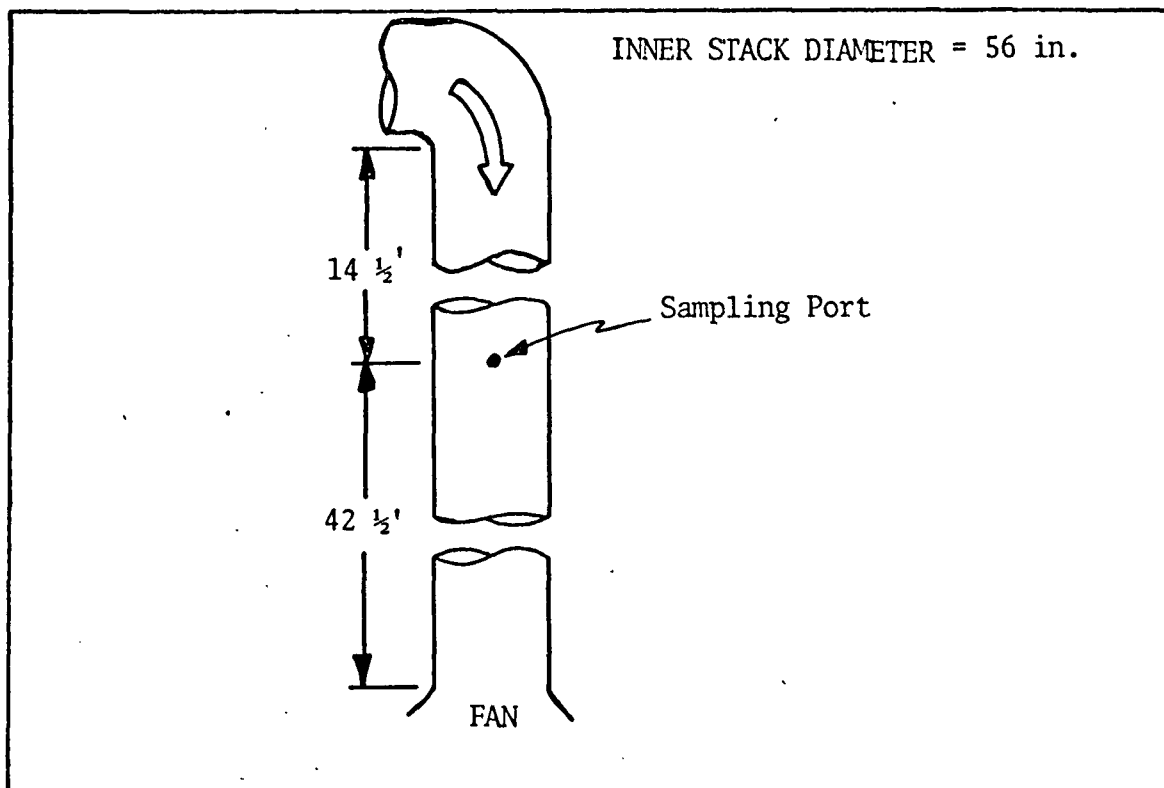
Sampling Point	Distance From Inner Wall (in.)
1	2 7/8
2	4 7/8
3	7 3/8
4	10 1/2
5	14 7/8
6	27
7	31 1/2
8	34 5/8
9	37
10	39 1/4

FIGURE 2
LOCATION OF PORT AND SAMPLING POINTS, STATION K
C. F. CHEMICALS, INC.



Sampling Point	Distance From Inner Wall (in)
1	2 3/8
2	4
3	5 7/8
4	7 7/8
5	10 1/8
6	12 3/4
7	16
8	20 5/8
9	33 3/8
10	38
11	41 1/4
12	43 7/8
13	46 1/8
14	48 1/8
15	50
16	51 5/8

FIGURE 3
LOCATION OF PORT AND SAMPLING POINTS,
STATION L
C. F. CHEMICALS, INC.



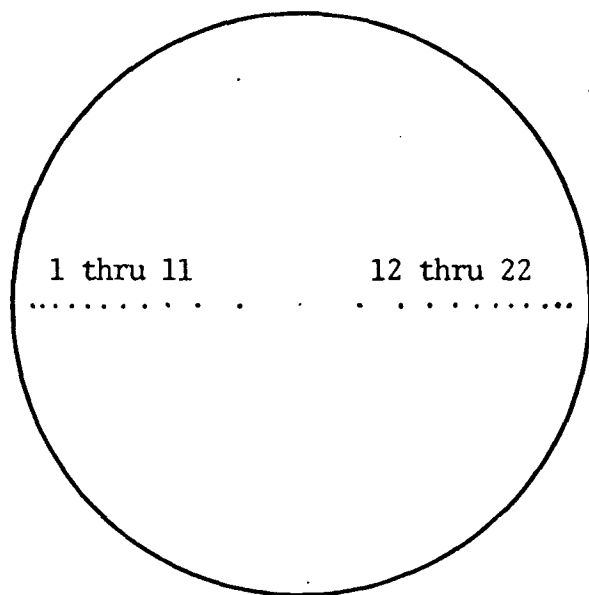
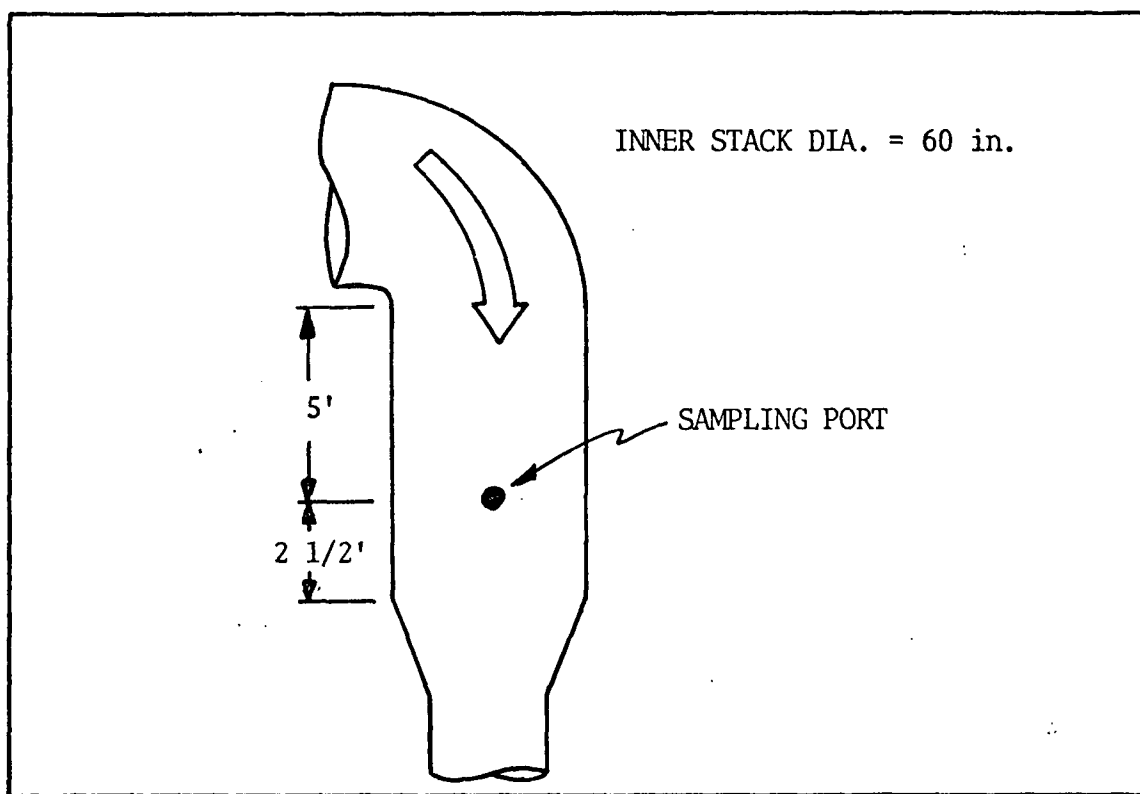
Sampling Point	Distance From Inner Wall (in.)
----------------	--------------------------------

1	2
2	3 3/8
3	4 7/8
4	6 1/2
5	8 1/4
6	10 1/8
7	12 1/4
8	14 5/8
9	17 5/8
10	22
11	34
12	38 3/8
13	41 3/8
14	43 3/4
15	45 7/8
16	47 3/4
17	49 1/2
18	51 1/8
19	52 5/8
20	54

FIGURE 4

LOCATION OF PORT AND SAMPLING POINTS,
STATION M

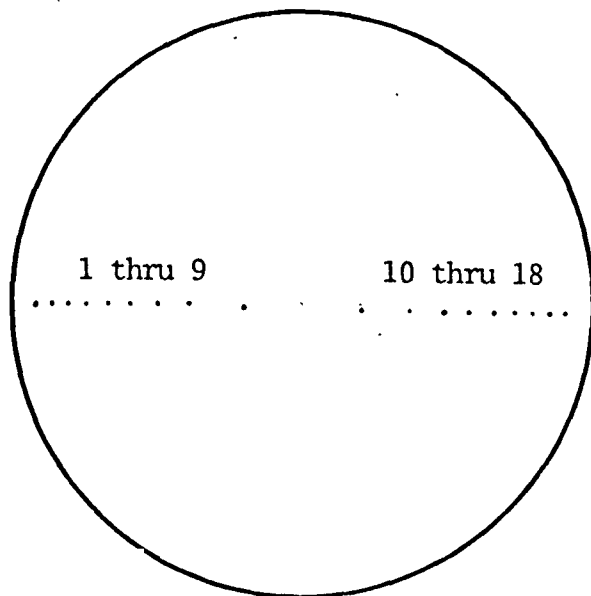
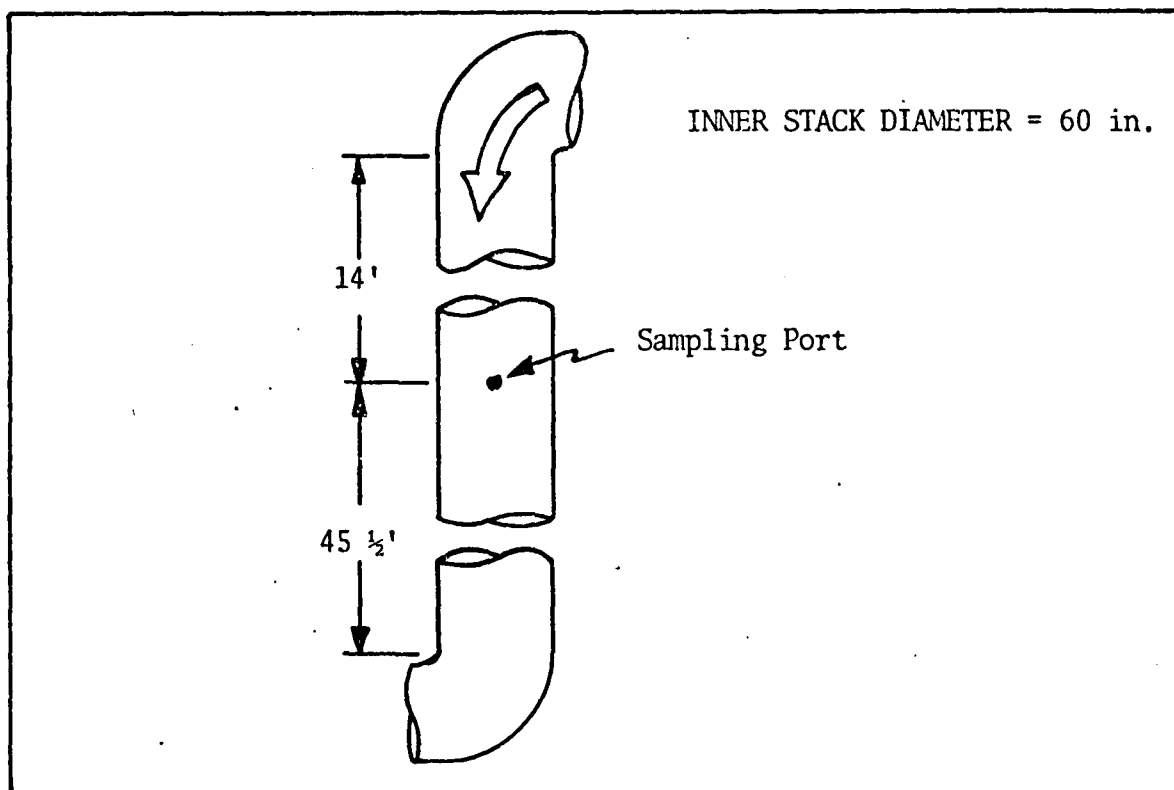
C. F. CHEMICALS, INC.



Sampling Point	Distance From Inner Wall (in.)
1	2 1/8
2	3 1/4
3	4 3/4
4	6 1/4
5	8
6	9 5/8
7	11 5/8
8	13 7/8
9	16 3/8
10	19 3/8
11	23 7/8
12	36 1/8
13	40 5/8
14	43 5/8
15	46 1/4
16	48 3/8
17	50 3/8
18	52
19	53 3/4
20	55 3/8
21	56 3/4
22	58

FIGURE 5

LOCATION OF PORT AND SAMPLING POINTS, STATION N
C. F. CHEMICALS, INC.

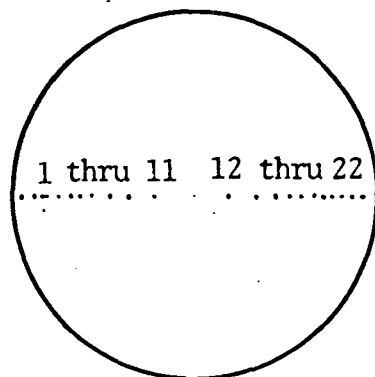
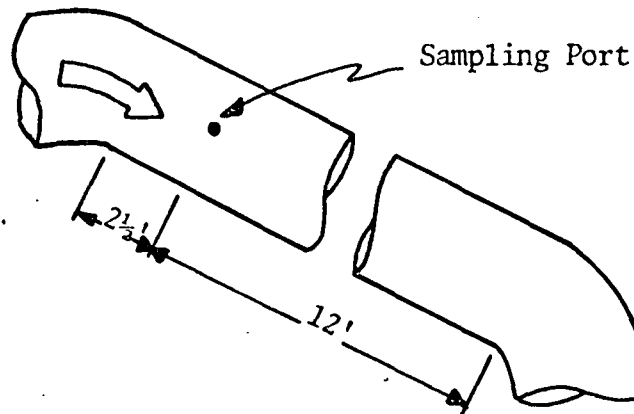


Sampling Point	Distance From Inner Wall (in)
1	2 3/8
2	4
3	5 7/8
4	7 3/4
5	9 7/8
6	12 1/4
7	15
8	18 3/8
9	24 1/4
10	36 3/4
11	41 5/8
12	45
13	47 3/4
14	50 1/8
15	52 1/4
16	54 1/4
17	56
18	57 5/8

FIGURE 6

LOCATION OF PORT AND SAMPLING POINTS,
STATION P
C. F. CHEMICALS, INC.

INNER STACK DIAMETER = 37 1/2 in.



Sampling Point	Distance From Inner Wall (in.)
1	1 1/4
2	2 1/8
3	2 7/8
4	3 7/8
5	4 7/8
6	6 1/8
7	7 1/4
8	8 5/8
9	10 1/4
10	12 1/8
11	14 7/8
12	22 5/8
13	25 3/8
14	27 3/8
15	28 7/8
16	30 1/4
17	31 1/2
18	32 5/8
19	33 5/8
20	34 5/8
21	35 1/2
22	36 3/8

FIGURE 7

LOCATION OF PORT AND SAMPLING POINTS,
STATION R
C. F. CHEMICALS, INC.

SAMPLING AND ANALYTICAL PROCEDURES

+

A. Preliminary Moisture Determination

The preliminary moisture content of the stack gases at each sampling site was determined by Method 4 of the Federal Register (Volume 36, Number 247, Part II, December 23, 1971).

The only significant difference between F. R. Method 4 and the method used was the configuration of the sampling train (see Figure 8). The sampling train used in these tests consisted of the first two midget impingers with five grams of distilled-deionized water followed by two dry midget impingers in place of a silica gel cartridge.

At sampling sites where liquid entrainment was a problem, the preliminary and final moisture contents were determined from wet and dry bulb thermometry. See Appendix B for the data used in determining the preliminary moisture content of the stack gases.

After completing the moisture run, the total impinger liquid plus water rinsings of the probe tip thorough the fourth impinger were placed in an eight ounce polyethylene container. The samples were held by EPA personnel for further analyses.

B. Preliminary Velocity Determination

Method two of the above mentioned Federal Register was used as a guide in determining the preliminary stack gas velocity for each source tested. The major difference was that only the maximum and minimum

velocity heads across each stack area were determined so that a proper nozzle size could be selected. During each of the three fluoride emission tests, velocity head readings were taken at points selected by using Method 1 of the Federal Register.

Stack pressure and temperature measurements were also made during the preliminary velocity determinations.

C. Sampling for Fluoride Emissions

The sampling procedure used for determining fluoride emissions was similar to Method 5 of the Federal Register. The major difference between the two methods was the configuration of the sampling train. The sampling train described in the Federal Register has a heated box containing the filter holder directly following the glass probe. The sampling train used in these tests contained no heated box and the filter holder was placed between the third and fourth impingers (between dry impinger and silica gel impinger) to prevent sample carry-over. Figure 9 is a schematic diagram of the sampling train used.

After the selection of the sampling site and the minimum number of sampling points per Method 2 of the above mentioned Federal Register, three separate test runs were performed. For each run, the required stack and sampling parameters were recorded on field data sheets. They are included in Appendix B. Readings were taken at each traverse point at least every five minutes, and when significant changes in stack parameters necessitated additional adjustments to maintain an isokinetic flow rate. Nomographs were used to aid in the rapid adjustment of the sampling

rate. The traverse points were selected to maintain at least one inch from the inner stack wall.

After each run, the liquid volume in the first three impingers was measured volumetrically and the silica gel was reweighed. The impinger liquid, the filter, plus the water washings of the probe and other sampling train components up to the silica gel were placed into polyethylene containers. During some runs the different sample fractions were placed in separate containers, while during others, all the recovered sample was placed into one container (See Appendix D). Field data sheets are included in Appendix B.

D. Sampling and Analytical Procedure for Ammonia

Ammonia was collected from the stack gas stream by passing the gas through three series-connected midget impingers containing 15 ml of 1N sulfuric acid. The sampling procedure was conducted per the EPA Officer and is very similar to the procedure described by Decker and Hogan in the U.S.P.H.S. publication "Determination of Ammonia in Stack Gas."

The apparatus consisted of a heated glass probe, midget impingers, pump, rotameter, and a dry gas test meter assembled as shown in Figure 10. Glass wool was placed in the end of the probe to act as a filter. Glass ball joint connectors were used between the probe and impingers. The first three impingers contained the absorbing reagent and the fourth impinger was left dry to collect any entrained liquid.

The sampling train was leak tested prior to sampling by plugging the inlet of the first impinger and letting the pump create a vacuum on the system. Any movement of the dry test meter was then recorded.

Due to the sensitivity of the analytical method only a small sample was required. The sampling rate was maintained at approximately

0.1 CFM for a 30-minute sampling time.

After each of the three sample runs, the total impinger liquid plus a distilled water rinsing of all four impingers was placed into an eight-ounce polyethylene jar for storage.

Field data sheets are contained in Appendix B.

E. Liquid and Product Grab Samples

Periodically, during each test run, grab samples of the raw materials, finished product, and scrubber liquid were taken, and the temperature and pH were determined at the site. On some occasions, the samples were split with the plant personnel so that comparative analyses could be performed.

F. Laboratory Analysis Procedures

Water soluble fluorides were done by a sulfuric acid distillation followed by the SPADNS-ZIRCONIUM LAKE METHOD. Water insoluble fluorides were first fused with NaOH followed by a sulfuric acid distillation then by the SPADNS-ZIRCONIUM LAKE METHOD.

Ammonia is quantitatively recovered as ammonia borate by using a modified kjeldahl distillation procedure. The ammonia samples were split with plant personnel. The analyses done by the Environmental Protection Agency are reported.

P_2O_5 analysis of the stack effluent was done by EPA personnel.

For more details of exact method used see Appendix C.

1. Nozzle (Optional)
2. Heated Glass Probe with Glass Wool as Filter
3. Ice Bath
4. Midget Impinger Containing 5 ml H_2O
5. Midget Impinger Containing 5 ml H_2O
6. Midget Impinger, Dry
7. Dry Midget Impinger
8. Flexible Sample Line
9. Drying Tube
10. Pump
11. Control Valve
12. Rotameter
13. Dry Test Meter
14. Thermometer

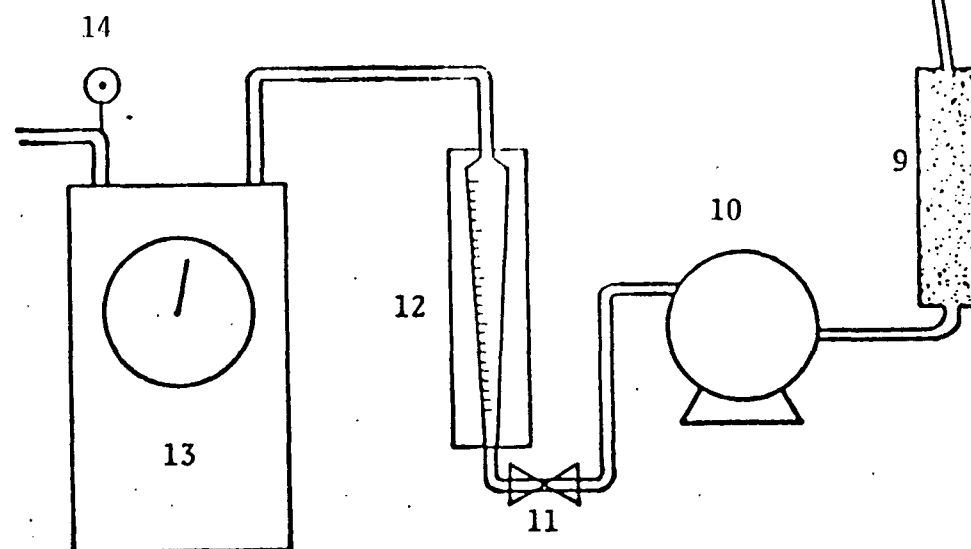


FIGURE 8

PRELIMINARY MOISTURE SAMPLING TRAIN

- 32
1. Nozzle
 2. Heated Glass Probe
 3. Glass Connector
 4. Ice Bath
 5. Impinger with 100 ml Distilled H₂O
 6. Impinger with 100 ml Distilled H₂O
 7. Impinger, Dry
 8. Filter Holder Containing No. 1 Whatman Filter
 9. Impinger with Silica Gel
 10. Thermometer
 11. Flexible Sample Line
 12. Vacuum Gauge
 13. Main Control Valve
 14. Air Tight Vacuum Pump
 15. By-pass Control Valve
 16. Thermometer
 17. Dry Test Meter
 18. Thermometer
 19. Calibrated Orifice
 20. Inclined Manometer
 21. "S" Type Pitot Tube
 22. Inclined Manometer

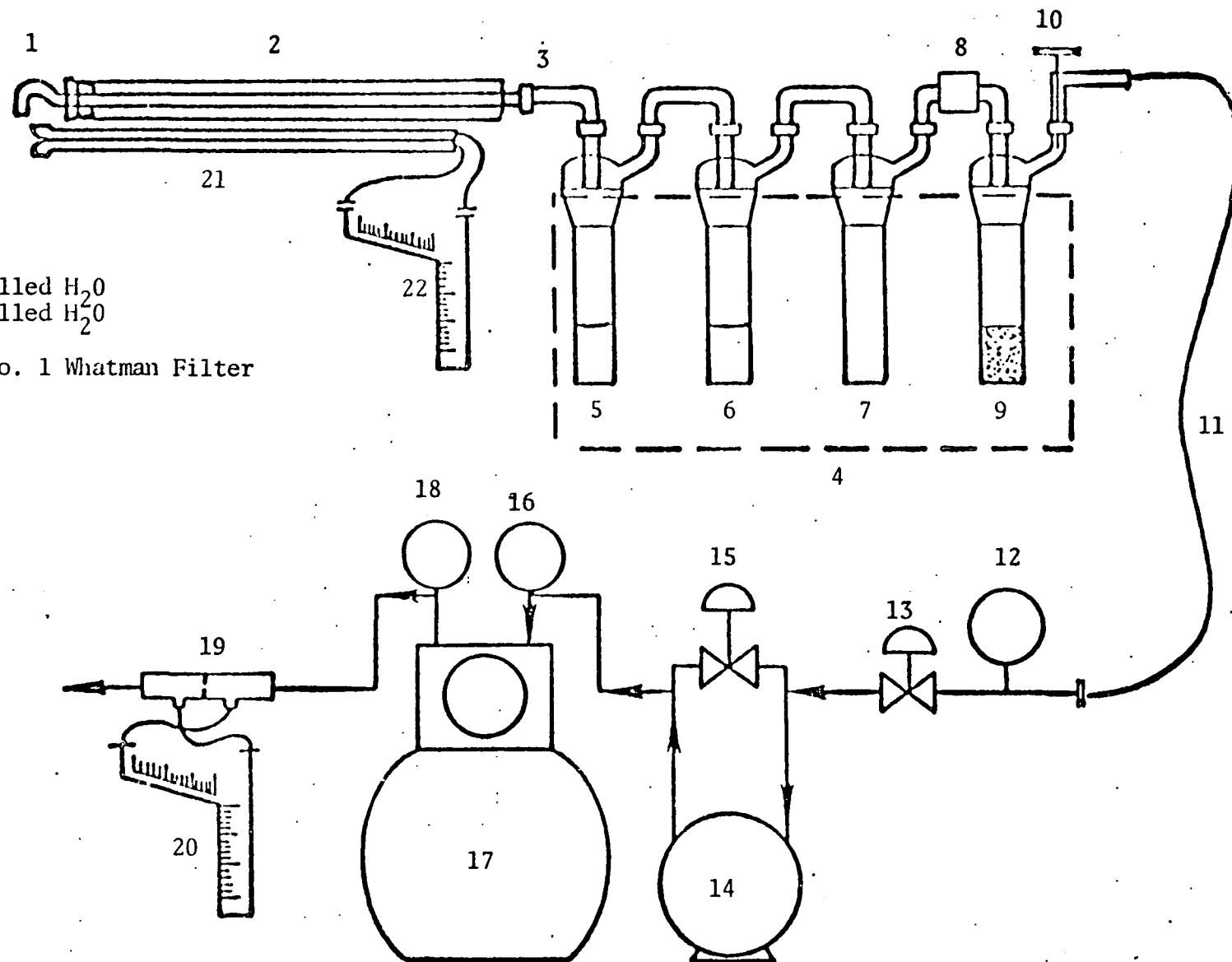


FIGURE 9
FLUORIDE SAMPLING TRAIN

1. Nozzle (Optional)
2. Heated Glass Probe with Glass Wool as Filter
3. Ice Bath
4. Midget Impingers Containing 15 ml $\text{1NH}_2\text{SO}_4$
5. Midget Impingers Containing 15 ml $\text{1NH}_2\text{SO}_4$
6. Midget Impingers Containing 15 ml $\text{1NH}_2\text{SO}_4$
7. Dry Midget Impinger
8. Flexible Sample Line
9. Drying Tube
10. Pump
11. Control Valve
12. Rotameter
13. Dry Test Meter
14. Thermometer

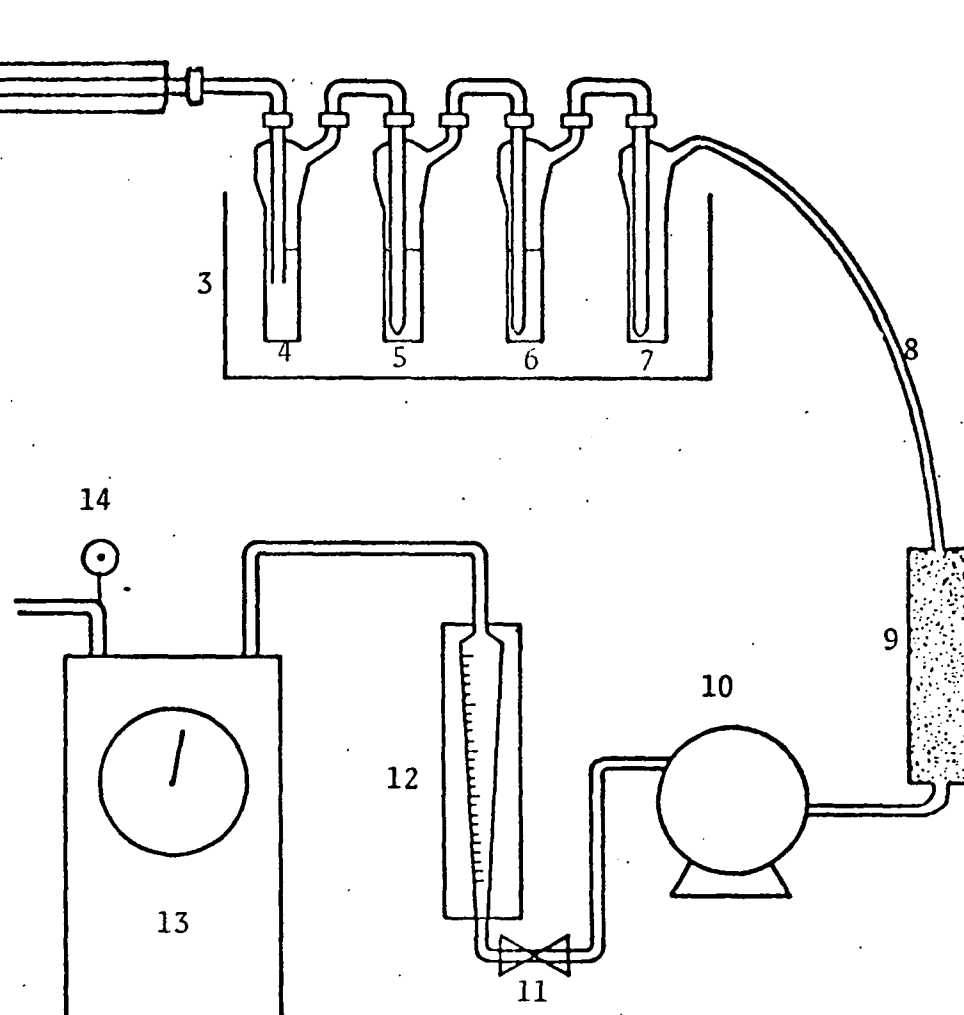


FIGURE 10
AMMONIA SAMPLING TRAIN

APPENDICES

APPENDIX A

Emission Calculations and Results

E.E.I. SOURCE SAMPLING NOMENCLATURE SHEET

- PB - Barometric pressure, inches Hg
 - PS - Stack pressure, inches Hg
 - As - Stack area, sq. ft.
 - AS' - Effective area of positive stack gas flow, sq. ft.
 - NPTS - Number of traverse points where the pitot velocity head was greater than zero
 - TS - Stack temperature, °R
 - TM - Meter temperature, °R
 - $\bar{H}$ - Average square root of velocity head, $\sqrt{\text{inches H}_2\text{O}}$
 - ΔH - Average meter orifice pressure differential, inches H₂O
 - AN - Sampling nozzle area, square feet
 - CP - S-type pitot tube correction factor
 - VM - Recorded meter volume sample, cubic feet (meter conditions)
 - VC - Condensate and silica gel increase in impingers, milliliters
 - Po - Pressure at the dry test meter orifice, $\left[\text{PB} + \frac{\Delta H}{13.6} \right]$ inches Hg
 - STP - Standard conditions, dry, 70°F, 29.92 inches Hg
- - - - -
- VWV - Conversion of condensate in milliliters to water vapor in cubic feet (STP)
 - VSTPD - Volume sampled, cubic feet (STP)
 - VT - Total water vapor volume and dry gas volume sampled, cubic feet (STP)
 - W - Moisture fraction of stack gas
 - FDA - Dry gas fraction
 - MD - Molecular weight of stack gas, lbs/lb-mole (dry conditions)
 - MS - Molecular weight of stack gas, lbs/lb-mole (stack conditions)
 - GS - Specific gravity of stack gas, referred to air
 - EA - Excess air, %
 - $\sqrt{H \times TS}$ - Average square root of velocity head times stack temperature
 - U - Stack gas velocity, feet per minute
 - QS - Stack gas flow rate, cubic feet per minute (stack conditions)
 - QD - Stack gas flow rate, cubic feet per minute (dry conditions)
 - QSTPD - Stack gas flow rate, cubic feet per minute (STP)
 - PISO - Percent isokinetic volume sampled (method described in Federal Register)

EQUATIONS FOR CALCULATING FLUORIDE EMISSIONS

$$VWV = (0.0474) \times (VC)$$

$$VSTPD = (17.71 \times (VM) \times (PB + \frac{\Delta H}{13.6}) \div TM$$

$$VT = (VWV) + (VSTPD)$$

$$W = (VWV) \div (VT)$$

$$FDA = (1.0) - (W)$$

FMOIST = Assumed moisture fraction

$$MD = (0.44 \times \% CO_2) + (0.32 \times \% O_2) + (0.28 \times \% N_2) + (0.28 \times \% CO)$$

$$MS = (MD \times FDA) + (18 \times W)$$

$$GS = (MS) \div (28.99)$$

$$EA = \left[(100) \times (\% O_2 - \frac{\% CO}{2}) \right] \div \left[(0.266 \times \% N_2) - (\% O_2 - \frac{\% CO}{2}) \right]$$

$$\underline{U} = (174) \times (CP) \times (\underline{H}) \times \sqrt{(TS \times 29.92) \div (GS \times PS)}$$

$$QS = (\underline{U}) \times (AS)$$

$$QD = (QS) \times (FDA)$$

$$QSTPD = (QD) \times (\frac{530}{29.92}) \times (\frac{PS}{TS})$$

$$PISO = (0.00267 \times VC \times TS) + (P_o \times TS \times VM \div TM) \div (Time \times \underline{U} \times PS \times AN)$$

Fluoride Emissions:

MG = Milligrams of fluoride from lab analysis

$$Grains/SCF = (0.01543) \times (MG) \div VSTPD$$

$$Grains/CF, Stack Cond. = (17.71) \times (PS) \times (FDA) \times (Grains/SCF) \div (TS)$$

$$Lbs/hour = (Grains/SCF) \times (0.00857) \times (QSTPD)$$

P₂O₅ Fed = Tons/hour, determined from plant data

$$Lbs/ton P_2O_5 Fed = (lbs/hour) \div (Tons/hour P_2O_5 Fed)$$

EQUATIONS FOR CALCULATING AMMONIA EMISSIONS

$$VSTPD = 17.71 \times VM \times (PB + \frac{\Delta H}{13.6}) \div TM$$

FDA = obtained from fluoride emission test

QSTPD = obtained from fluoride emission test

Ammonia Emissions:

Mg = Milligrams of NH_3 , determined from lab analysis

$$\text{Grains/SCF} = (0.01543) \times (MG) \div VSTPD$$

$$\text{Grains/CF, Stack Cond.} = (17.71) \times (PS) \times (FDA) \times (\text{Grains/SCF}) \div TS$$

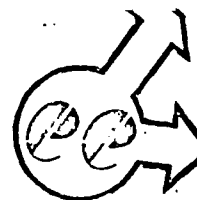
$$\text{Lbs/hour} = (\text{Grains/SCF}) \times (0.00857) \times (QSTPD)$$

NH_3 Fed = Tons/hour, determined from plant data

$$\text{Lbs/ton } NH_3 \text{ Fed} = (\text{lbs/hour}) \div (\text{tons/hour } NH_3 \text{ Fed})$$

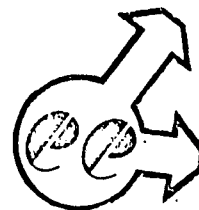
FLUORIDE EMISSIONS

SOURCE TEST DATA



TEST NO. _____ NO. OF RUNS 3
 NAME OF FIRM C.F. CHEMICALS
 LOCATION OF PLANT BARTOW FLORIDA
 TYPE OF PLANT D.A.P.
 CONTROL EQUIPMENT _____
 SAMPLING POINT LOCATION STATION K REACTOR SCRUBBER OUTLET
 POLLUTANTS SAMPLED _____

	1	2	3
1) RUN NO.			
2) DATE	12/16/71	12/18/71	12/20/71
3) TIME BEGAN	16:20	13:45	18:00
4) TIME END	18:20	15:45	20:00
5) BAROMETRIC PRESSURE, "Hg ABSOLUTE	30	30	30
6) METER ORIFICE PRESSURE DROP, "H ₂ O	2.29	3.49	2.22
7) VOL DRY GAS @ METER CONDITIONS, ft ³	108.461	134.054	104.333
8) AVERAGE GAS METER TEMPERATURE, °F	96.1	79.4	81.8
9) VOL DRY GAS @ S.T.P.*, ft ³	104.233	133.2	102.895
10) TOTAL H ₂ O COLLECTED, ml	642.3	1037.1	670.5
11) VOL WATER VAPOR COLL. @ S.T.P., ft ³	30.45	49.16	31.78
12) STACK GAS MOISTURE, % VOLUME	22.6	27	23.6
13) ASSUMED STACK GAS MOISTURE, % VOLUME	8	22	22
14) % CO ₂	0	0	0
15) % O ₂	19.4	21	20.6
16) % CO	0	0	0
17) % N ₂	80.6	79	79.4
18) % EXCESS AIR	951	150000	3958
19) MOLECULAR WT. OF STACK GAS, DRY	28.78	28.84	28.82
20) MOLECULAR WT. OF STACK GAS, STACK COND.	26.34	25.92	26.27
21) STACK GAS SP. GRAVITY, REF. TO AIR	0.91	0.89	0.91
22) AVG VEL. HEAD OF STACK GAS, "H ₂ O	0.949	1.461	0.917
23) AVERAGE STACK GAS TEMPERATURE, °F	164	169.5	170
24) PITOT CORRECTION FACTOR	0.83	0.83	0.83
25) STACK PRESSURE, "Hg ABSOLUTE	29	29	29
26) STACK GAS VEL @ STACK COND., fpm	3647.1	5689	3547.9
27) STACK AREA, ft ²	9.62	9.62	9.62
28) STACK GAS FLOW RATE @ S.T.P., scfm	23066	33660	21940
29) NET TIME OF TEST, min.	120	120	120
30) SAMPLING NOZZLE DIAMETER, in.	0.25	0.25	0.25
31) PERCENT ISOKINETIC	109.6	96	113.7
32) FLUORIDE - WATER SOLUBLE, MG	67	147	57
33) FLUORIDE - TOTAL, MG	67.67	147.77	64.3
34) FLUORIDE - WATER SOLUBLE, GR/SCF	0.0095	0.0169	0.0084
35) FLUORIDE - TOTAL, GR/SCF	0.0096	0.017	0.0095
36) FLUORIDE - WATER SOL. GR/CF STK COND.	0.0061	0.0101	0.0052
37) FLUORIDE - TOTAL GR/CF STK COND.	0.0061	0.0101	0.0059
38) FLUORIDE - WATER SOLUBLE, LB/HOUR	1.8805	4.8714	1.5819
39) FLUORIDE - TOTAL, LB/HOUR	1.8993	4.8969	1.7845
41) FLUORIDE - WATER SOL. LB/TON P2O5 FED.	0.0646	0.1949	0.0625
42) FLUORIDE - TOTAL, LBS/TON P2O5 FED.	0.0653	0.1959	0.0705

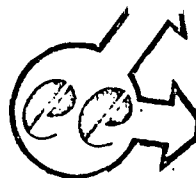


SOURCE TEST DATA

TEST NO. _____ NO. OF RUNS 3
NAME OF FIRM C. F. CHEMICALS
LOCATION OF PLANT BARTOW FLORIDA
TYPE OF PLANT D.A.P.
CONTROL EQUIPMENT _____
SAMPLING POINT LOCATION STATION L DRYER SCRUBBER INLET
POLLUTANTS SAMPLED _____

	1	2	3
1) RUN NO.			
2) DATE	12/16/71	12/18/71	12/20/71
3) TIME BEGAN	16:20	13:50	13:05
4) TIME END	18:20	15:50	20:05
5) BAROMETRIC PRESSURE, "Hg ABSOLUTE	30	30	30
6) METER ORIFICE PRESSURE DROP, "H ₂ O	1.75	1.72	1.62
7) VOL DRY GAS @ METER CONDITIONS, ft ³	94.054	93.982	83.097
8) AVERAGE GAS METER TEMPERATURE, °F	129	107.4	114.4
9) VOL DRY GAS @ S.T.P.*, ft ³	85.228	88.388	81.827
10) TOTAL H ₂ O COLLECTED, ml	435.6	215.9	170.1
11) VOL WATER VAPOR COLL. @ S.T.P., ft ³	20.65	10.23	8.06
12) STACK GAS MOISTURE, % VOLUME	19.5	10.4	9
13) ASSUMED STACK GAS MOISTURE, % VOLUME	9	18	18
14) % CO ₂	0	0	
15) % O ₂	20.4	20.5	
16) % CO	0	0	
17) % N ₂	79.6	79.5	
18) % EXCESS AIR	2637	3168	0
19) MOLECULAR WT. OF STACK GAS, DRY	23.32	28.82	28.99
20) MOLECULAR WT. OF STACK GAS, STACK COND.	26.71	27.7	28
21) STACK GAS SP. GRAVITY, REF. TO AIR	0.92	0.96	0.97
22) AVG VEL. HEAD OF STACK GAS, "H ₂ O	0.749	0.811	0.765
23) AVERAGE STACK GAS TEMPERATURE, °F	160.1	149.6	151.1
24) PITOT CORRECTION FACTOR	0.83	0.83	0.83
25) STACK PRESSURE, "Hg ABSOLUTE	30	30	30
26) STACK GAS VEL @ STACK COND., fpm	2801.6	2955.2	2776.1
27) STACK AREA, ft ²	15.9	15.9	15.9
28) STACK GAS FLOW RATE @ S.T.P., scfm	30655	36625	34855
29) NET TIME OF TEST, min.	120	120	120
30) SAMPLING NOZZLE DIAMETER, in.	0.25	0.25	0.25
31) PERCENT ISOKINETIC	107.8	93.6	91
32) FLUORIDE - WATER SOLUBLE, MG	154	91	22.6
33) FLUORIDE - TOTAL, MG	216	141	37.9
34) FLUORIDE - WATER SOLUBLE, GR/SCF	0.0252	0.0149	0.004
35) FLUORIDE - TOTAL, GR/SCF	0.0354	0.0231	0.0066
36) FLUORIDE - WATER SOL. GR/CF STK COND.	0.0174	0.0116	0.0031
37) FLUORIDE - TOTAL GR/CF STK COND.	0.0244	0.018	0.0052
38) FLUORIDE - WATER SOLUBLE, LB/HOUR	6.6244	4.6803	1.1801
39) FLUORIDE - TOTAL, LB/HOUR	9.2914	7.2519	1.979
41) FLUORIDE - WATER SOL. LB/TON P205 FED.	0.2276	0.1872	0.0466
42) FLUORIDE - TOTAL, LBS/TON P205 FED.	0.3193	0.2901	0.0782

SOURCE TEST DATA

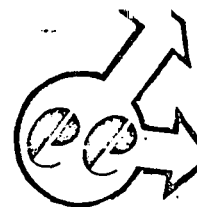


TEST NO. _____ NO. OF RUNS 3
 NAME OF FIRM C. F. CHEMICALS
 LOCATION OF PLANT BARTOW FLORIDA
 TYPE OF PLANT D.A.P.
 CONTROL EQUIPMENT _____
 SAMPLING POINT LOCATION STATION M DRYER SCRUBBER OUTLET
 POLLUTANTS SAMPLED _____

	1	2	3
1) RUN NO.	12/16/71	12/18/71	12/20/71
2) DATE	17:30	13:45	18:00
3) TIME BEGAN	19:12	15:33	19:36
4) TIME END	30	30	30
5) BAROMETRIC PRESSURE, "Hg ABSOLUTE	2.32	1.8	1.88
6) METER ORIFICE PRESSURE DROP, "H ₂ O	83.382	80.732	75.425
7) VOL DRY GAS @ METER CONDITIONS, ft ³	93.4	76.6	82
8) AVERAGE GAS METER TEMPERATURE, °F	80.528	80.301	74.294
9) VOL DRY GAS @ S.T.P.*, ft ³	225	225	262
10) TOTAL H ₂ O COLLECTED, ml	10.67	10.67	12.42
11) VOL WATER VAPOR COLL. @ S.T.P., ft ³	11.7	11.7	14.3
12) STACK GAS MOISTURE, %VOLUME	13.9	15	9.7
13) ASSUMED STACK GAS MOISTURE, %VOLUME	0.6	0	0
14) % CO ₂	19.8	20	20.3
15) % O ₂	0	0	0
16) % CO	79.6	80	79.7
17) % N ₂	1441	1563	2255
18) % EXCESS AIR	28.89	28.8	28.81
19) MOLECULAR WT. OF STACK GAS, DRY	27.61	27.53	27.26
20) MOLECULAR WT. OF STACK GAS, STACK COND.	0.95	0.95	0.94
21) STACK GAS SP. GRAVITY, REF. TO AIR	0.779	0.705	0.641
22) AVG VEL. HEAD OF STACK GAS, "H ₂ O	132	111	110.3
23) AVERAGE STACK GAS TEMPERATURE, °F	0.83	0.83	0.83
24) PITOT CORRECTION FACTOR	28.1	28.1	28.2
25) STACK PRESSURE, "Hg ABSOLUTE	2893.8	2576.1	2349.9
26) STACK GAS VEL @ STACK COND., fpm	17.1	17.1	17.1
27) STACK AREA, ft ²	39130	36103	31979
28) STACK GAS FLOW RATE @ S.T.P., scfm	102	102	96
29) NET TIME OF TEST, min.	0.25	0.25	0.25
30) SAMPLING NOZZLE DIAMETER, in.	107.8	116.5	128.8
31) PERCENT ISOKINETIC	2.4	8.1	1.2
32) FLUORIDE - WATER SOLUBLE, MG	2.466	8.42	1.41
33) FLUORIDE - TOTAL, MG	0.0004	0.0015	0.0002
34) FLUORIDE - WATER SOLUBLE, GR/SCF	0.0005	0.0016	0.0003
35) FLUORIDE - TOTAL, GR/SCF	0.0003	0.0012	0.0002
36) FLUORIDE - WATER SOL. GR/CF STK COND.	0.0003	0.0012	0.0002
37) FLUORIDE - TOTAL GR/CF STK COND.	0.1486	0.4781	0.0671
38) FLUORIDE - WATER SOLUBLE, LB/HOUR	0.1527	0.5054	0.0789
39) FLUORIDE - TOTAL, LB/HOUR	0.0051	0.0191	0.0027
41) FLUORIDE - WATER SOL. LB/TON P2O5 FED.	0.0052	0.0202	0.0031
42) FLUORIDE - TOTAL, LBS/TON P2O5 FED.			

* DRY. 70 °F. 29.92 in. Hg

SOURCE TEST DATA

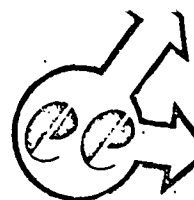


TEST NO. _____ NO. OF RUNS 3
 NAME OF FIRM C. F. CHEMICALS
 LOCATION OF PLANT BARTOW FLORIDA
 TYPE OF PLANT D.A.P.
 CONTROL EQUIPMENT _____
 SAMPLING POINT LOCATION STATION N COOLER SCRUBBER INLET
 POLLUTANTS SAMPLED _____

	1	2	3
1) RUN NO.			
2) DATE	12/16/71	12/18/71	12/20/71
3) TIME BEGAN	16:20	13:50	18:00
4) TIME END	18:21	15:51	20:01
5) BAROMETRIC PRESSURE, "Hg ABSOLUTE	30	30	30
6) METER ORIFICE PRESSURE DROP, "H ₂ O	1.3	1.22	1.75
7) VOL DRY GAS @ METER CONDITIONS, ft ³	80.579	74.567	86.616
8) AVERAGE GAS METER TEMPERATURE, °F	108.7	76.7	84.7
9) VOL DRY GAS @ S.T.P.*, ft ³	75.538	74.057	84.862
10) TOTAL H ₂ O COLLECTED, ml	42.8	33.1	45.8
11) VOL WATER VAPOR COLL. @ S.T.P., ft ³	2.03	1.57	2.17
12) STACK GAS MOISTURE, %VOLUME	2.6	2.1	2.5
13) ASSUMED STACK GAS MOISTURE, %VOLUME	5	3	3
14) % CO ₂	0	0	0
15) % O ₂	19.8	20.3	20
16) % CO	0	0	0
17) % N ₂	80.2	79.7	80
18) % EXCESS AIR	1291	2255	1563
19) MOLECULAR WT. OF STACK GAS, DRY	28.79	28.81	28.8
20) MOLECULAR WT. OF STACK GAS, STACK COND.	28.51	28.59	29.53
21) STACK GAS SP. GRAVITY, REF. TO AIR	0.98	0.99	0.98
22) AVG VEL. HEAD OF STACK GAS, "H ₂ O	0.596	0.566	0.685
23) AVERAGE STACK GAS TEMPERATURE, °F	140	140	140
24) PITOT CORRECTION FACTOR	0.83	0.83	0.83
25) STACK PRESSURE, "Hg ABSOLUTE	29.71	29.71	29.71
26) STACK GAS VEL @ STACK COND., fpm	2132.5	2023.8	2450.3
27) STACK AREA, ft ²	19.63	19.63	19.63
28) STACK GAS FLOW RATE @ S.T.P., scfm	36019	34373	41447
29) NET TIME OF TEST, min.	121	121	121
30) SAMPLING NOZZLE DIAMETER, in.	0.25	0.25	0.25
31) PERCENT ISOKINETIC	100.5	103.3	98.1
32) FLUORIDE - WATER SOLUBLE, MG	34	25	31
33) FLUORIDE - TOTAL, MG	64.2	43.5	48.6
34) FLUORIDE - WATER SOLUBLE, GR/SCF	0.0065	0.0052	0.0055
35) FLUORIDE - TOTAL, GR/SCF	0.0123	0.009	0.0086
36) FLOURIDE - WATER SOL. GR/CF STK COND.	0.0055	0.0044	0.0047
37) FLOURIDE - TOTAL GR/CF STK COND.	0.0105	0.0077	0.0074
38) FLUORIDE - WATER SOLUBLE, LB/HOUR	2.0058	1.5209	1.9578
39) FLUORIDE - TOTAL, LB/HOUR	3.7874	2.6464	3.0693
41) FLOURIDE - WATER SOL. LB/TON P205 FED.	0.0689	0.0608	0.0774
42) FLUORIDE - TOTAL, LBS/TON P205 FED.	0.1302	0.1059	0.1213

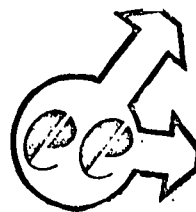
* DRY. 70 °F. 29.92 in. Hg

SOURCE TEST DATA



TEST NO. _____ NO. OF RUNS 3
 NAME OF FIRM C. F. CHEMICALS
 LOCATION OF PLANT BARTOW FLORIDA
 TYPE OF PLANT D.A.P.
 CONTROL EQUIPMENT _____
 SAMPLING POINT LOCATION STATION P COOLER SCRUBBER OUTLET
 POLLUTANTS SAMPLED _____

	1	2	3
1) RUN NO.			
2) DATE	12/16/71	12/18/71	12/20/71
3) TIME BEGAN	16:32	13:46	13:00
4) TIME END	18:29	15:43	19:57
5) BAROMETRIC PRESSURE, "Hg ABSOLUTE	30	30	30
6) METER ORIFICE PRESSURE DROP, "H ₂ O	2.23	2.53	3.31
7) VOL DRY GAS @ METER CONDITIONS, ft ³	90.39	105.346	123.14
8) AVERAGE GAS METER TEMPERATURE, °F	116.4	104.7	117.5
9) VOL DRY GAS @ S.T.P.*, ft ³	83.789	99.759	114.24
10) TOTAL H ₂ O COLLECTED, ml	227.5	221.5	190
11) VOL WATER VAPOR COLL. @ S.T.P., ft ³	10.78	10.5	9.29
12) STACK GAS MOISTURE, % VOLUME	11.4	9.5	7.5
13) ASSUMED STACK GAS MOISTURE, % VOLUME	10.5	11.5	11.5
14) % CO ₂	0	0	0
15) % O ₂	19.5	20.6	20.3
16) % CO	0	0	0
17) % N ₂	80.5	79.4	79.7
18) % EXCESS AIR	1019	3958	2255
19) MOLECULAR WT. OF STACK GAS, DRY	23.78	23.82	23.31
20) MOLECULAR WT. OF STACK GAS, STACK COND.	27.55	27.79	28
21) STACK GAS SP. GRAVITY, REF. TO AIR	0.95	0.96	0.97
22) AVG VEL. HEAD OF STACK GAS, "H ₂ O	0.813	0.375	0.90
23) AVERAGE STACK GAS TEMPERATURE, °F	124.1	100	95.1
24) PITOT CORRECTION FACTOR	0.83	0.83	0.83
25) STACK PRESSURE, "Hg ABSOLUTE	28.7	28.7	28.7
26) STACK GAS VEL @ STACK COND., fpm	2972.6	3117.9	3499.0
27) STACK AREA, ft ²	19.63	19.63	19.63
28) STACK GAS FLOW RATE @ S.T.P., scfm	46921	52423	60075
29) NET TIME OF TEST, min.	117	117	117
30) SAMPLING NOZZLE DIAMETER, in.	0.25	0.25	0.25
31) PERCENT ISOKINETIC	91.6	97.6	90.6
32) FLUORIDE - WATER SOLUBLE, MG	2.8	4.6	2.7
33) FLUORIDE - TOTAL, MG	2.8	4.671	2.751
34) FLUORIDE - WATER SOLUBLE, GR/SCF	0.0005	0.0007	0.0003
35) FLUORIDE - TOTAL, GR/SCF	0.0005	0.0007	0.0003
36) FLOURIDE - WATER SOL. GR/CF STK COND.	0.0004	0.0006	0.0003
37) FLOURIDE - TOTAL GR/CF STK COND.	0.0004	0.0006	0.0003
38) FLUORIDE - WATER SOLUBLE, LB/HOUR	0.1918	0.3021	0.1756
39) FLUORIDE - TOTAL, LB/HOUR	0.1918	0.3068	0.1789
41) FLOURIDE - WATER SOL. LB/TON P205 FED.	0.0066	0.0121	0.0069
42) FLUORIDE - TOTAL, LBS/TON P205 FED.	0.0066	0.0123	0.0071



SOURCE TEST DATA

TEST NO. _____ NO. OF RUNS _____ 3
NAME OF FIRM C. F. CHEMICALS
LOCATION OF PLANT BARTOW FLORIDA
TYPE OF PLANT D.A.P.
CONTROL EQUIPMENT _____
SAMPLING POINT LOCATION STATION R REACTOR SCRUBBER INLET
POLLUTANTS SAMPLED _____

	1	2	3
1) RUN NO.	12/16/71	12/18/71	12/20/71
2) DATE	16:35	13:45	18:05
3) TIME BEGAN	18:40	15:38	19:59
4) TIME END	30	30	30
5) BAROMETRIC PRESSURE, "Hg ABSOLUTE	4.04	2.65	2.34
6) METER ORIFICE PRESSURE DROP, "H ₂ O	126.2	91.153	86.1
7) VOL DRY GAS @ METER CONDITIONS, ft ³	102.8	73.3	85.8
8) AVERAGE GAS METER TEMPERATURE, °F	120.332	91.427	84.318
9) VOL DRY GAS @ S.T.P.*, ft ³	1039	834.6	856
10) TOTAL H ₂ O COLLECTED, ml	49.25	39.56	40.57
11) VOL WATER VAPOR COLL. @ S.T.P., ft ³	29	30.2	32.5
12) STACK GAS MOISTURE, %VOLUME	28	0	35
13) ASSUMED STACK GAS MOISTURE, %VOLUME	0	0	0.7
14) % CO ₂	19.8	20.7	19.8
15) % O ₂	0	0	0
16) % CO	80.2	79.3	79.5
17) % N ₂	1291	5256	1470
18) % EXCESS AIR	28.79	28.83	28.9
19) MOLECULAR WT. OF STACK GAS, DRY	25.66	25.56	25.36
20) MOLECULAR WT. OF STACK GAS, STACK COND.	0.89	0.88	0.87
21) STACK GAS SP. GRAVITY, REF. TO AIR	1.106	1.078	1.025
22) AVG VVEL. HEAD OF STACK GAS, "H ₂ O	171.6	171.3	173.4
23) AVERAGE STACK GAS TEMPERATURE, °F	0.83	0.83	0.83
24) PITOT CORRECTION FACTOR	29 x	29 x	29 x
25) STACK PRESSURE, "Hg ABSOLUTE	4337.9	4231.6	4047.9
26) STACK GAS VEL @ STACK COND., fpm	7.67	7.67	7.67
27) STACK AREA, ft ²	19812	19019	17540
28) STACK GAS FLOW RATE @ S.T.P., scfm	110	110	110
29) NET TIME OF TEST, min.	0.25	0.25	0.25
30) SAMPLING NOZZLE DIAMETER, in.	128.1	101.4	101.4
31) PERCENT ISOKINETIC			
32) FLUORIDE - WATER SOLUBLE, MG	143	71	319
33) FLUORIDE - TOTAL, MG	164.4	91.3	373
34) FLUORIDE - WATER SOLUBLE, GR/SCF	0.0175	0.012	0.0571
35) FLUORIDE - TOTAL, GR/SCF	0.0201	0.0154	0.0667
36) FLOURIDE - WATER SOL. GR/CF STK COND.	0.0101	0.0068	0.0312
37) FLOURIDE - TOTAL GR/CF STK COND.	0.0116	0.0088	0.0365
38) FLUORIDE - WATER SOLUBLE, LB/HOUR	2.9628	1.9551	8.5767
39) FLUORIDE - TOTAL, LB/HOUR	3.4062	2.5141	10.0285
41) FLOURIDE - WATER SOL. LB/TON P205 FED.	0.1018	0.0782	0.339
42) FLUORIDE - TOTAL, LBS/TON P205 FED.	0.1171	0.1006	0.3964

AMMONIA EMISSIONS

AMMONIA EMISSIONS DATA

PLANT C. F. CHEMICALS, INC. BARTON, FLA.

STACK D.A.P. HO. 3 STATION K

Run No.	1	2	3
Date	12/16/71	12/18/71	12/20/71
Time Started	18:55	16:05	20:15
Time Ended	19:25	16:35	20:45
Barometric Pressure, "Hg	30	30	30
Stack Pressure, "Hg	29	29	29
Final Meter Reading Ft ³	11.711	14.824	17.751
Initial Meter Reading Ft ³	8.439	11.725	14.824
Meter Volume (meter cond. Ft ³)	3.272	3.099	2.927
Gas Volume Sampled, *Ft ³	3.133	3.0329	2.8541
Meter Temperature °F	95	83	85
Stack Temperature °F	164	170	170
Average Gas Flow Rate, *Ft ³ /min	23066	33660	21940
Ammonia, mg	1.3	1.8	0.3
Ammonia lbs/hr	1.2632	2.6366	0.3008
Ammonia lb/ton NH ₃ fed	0.27461	0.23541	0.0029267
Ammonia gr/SCF	0.0063486	0.0090804	0.0016
Ammonia gr/CF Stack Cond.	0.0040453	0.0054051	0.0010

* Dry, 70°F, 29.92 "Hg



environmental engineering, inc.

AMMONIA EMISSIONS DATA

PLANT C.F. CHEMICALS, INC. BARTON, FLA.

STACK D.A.P. NO. 3 STATION L

Run No.	1	2	3
Date	12/16/71	12/18/71	12/20/71
Time Started	19:00	16:30	20:40
Time Ended	19:30	17:00	21:10
Barometric Pressure, "Hg	30	30	30
Stack Pressure, "Hg	29.7	29.7	29.7
Final Meter Reading Ft ³	158.44	258.1	353.57
Initial Meter Reading Ft ³	155.47	255.11	350.57
Meter Volume (meter cond. Ft ³)	2.97	2.989	3
Gas Volume Sampled, *Ft ³	2.7306	2.8263	2.7582
Meter Temperature °F	118	102	118
Stack Temperature °F	160	150	151
Average Gas Flow Rate, *Ft ³ /min	30655	36625	34855
Ammonia, mg	170.5	126.7	160.3
Ammonia lbs/hr	252.62	216.69	267.35
Ammonia lb/ton NH ₃ fed	54.918	19.347	25.707
Ammonia gr/SCF	0.95533	0.68587	0.88919
Ammonia gr/CF Stack Cond.	0.65257	0.53002	0.69673

* Dry, 70°F, 29.92 "Hg



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AMMONIA EMISSIONS DATA

PLANT C. F. CHEMICALS, INC. BARTON, FLA.

STACK D.A.P. NO. 3 STATION M

Run No.	1	2	3
Date	12/16/71	12/18/71	12/20/71
Time Started	19:00	16:00	20:00
Time Ended	19:30	16:30	20:30
Barometric Pressure, "Hg	30	30	30
Stack Pressure, "Hg	28.1	28.1	28.1
Final Meter Reading Ft ³	96.437	100.53	103.58
Initial Meter Reading Ft ³	93.253	97.4	100.57
Meter Volume (meter cond. Ft ³)	3.184	3.13	3.014
Gas Volume Sampled, *Ft ³	3.0487	3.1032	2.9497
Meter Temperature °F	95	76	83
Stack Temperature °F	132	111	111
Average Gas Flow Rate, *Ft ³ /min	39130	36103	31979
Ammonia, mg	0.04	2	1
Ammonia lbs/hr	0.067758	3.0709	1.4308
Ammonia lb/ton NH ₃ fed	0.01473	0.27419	0.13758
Ammonia gr/SCF	0.00020074	0.0098607	0.005187
Ammonia gr/CF Stack Cond.	0.00014904	0.0075902	0.0038751

* Dry, 70°F, 29.92 "Hg



environmental engineering, inc.

AMMONIA EMISSIONS DATA

PLANT C.F. CHEMICALS, INC. BARTON, FLA.

STACK D.A.P. HO. 3 STATION N

Run No.	1	2	3
Date	12/16/71	12/18/71	12/20/71
Time Started	19:00	16:03	20:05
Time Ended	19:30	16:33	20:35
Barometric Pressure, "Hg	30	30	30
Stack Pressure, "Hg	29.7	29.7	29.7
Final Meter Reading Ft ³	3.52	7.159	10.291
Initial Meter Reading Ft ³	0.61	3.543	7.17
Meter Volume (meter cond. Ft ³)	2.91	3.616	3.121
Gas Volume Sampled, *Ft ³	2.8117	3.5194	3.0266
Meter Temperature °F	90	86	88
Stack Temperature °F	140	140	140
Average Gas Flow Rate, *Ft ³ /min	36019	34373	41447
Ammonia, mg	23.2	0.05	0.1
Ammonia lbs/hr	39.225	0.06445	0.18074
Ammonia lb/ton NH ₃ fed	8.5272	0.0057545	0.017379
Ammonia gr/SCF	0.12624	0.00021737	0.00050553
Ammonia gr/CF Stack Cond.	0.10782	0.00018659	0.00043218

* Dry, 70°F, 29.92 "Hg



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AMMONIA EMISSIONS DATA

PLANT C.F. CHEMICALS, INC. BARTON, FLA.

STACK D.A.P. NO. 3 STATION P

Run No.	1	2	3
Date	12/16/71	12/18/71	12/20/71
Time Started	19:45	16:15	20:20
Time Ended	20:15	16:45	20:50
Barometric Pressure, "Hg	30	30	30
Stack Pressure, "Hg	28.7	28.7	28.7
Final Meter Reading Ft ³	486.88	605.37	732.72
Initial Meter Reading Ft ³	483.54	601.32	728.81
Meter Volume (meter cond. Ft ³)	3.338	4.047	3.902
Gas Volume Sampled, *Ft ³	3.179	3.7731	3.5568
Meter Temperature °F	98	110	123
Stack Temperature °F	124	100	95
Average Gas Flow Rate, *Ft ³ /min	46921	52423	60675
Ammonia, mg	1.6	1	0.2
Ammonia lbs/hr	3.1168	1.8337	0.45029
Ammonia lb/ton NH ₃ fed	0.67756	0.16373	0.043297
Ammonia gr/SCF	0.0077006	0.0040551	0.00086033
Ammonia gr/CF Stack Cond.	0.0059394	0.0033316	0.00072897

* Dry, 70°F, 29.92 "Hg



environmental engineering, inc.

AMMONIA EMISSIONS DATA

PLANT C.F. CHEMICALS, INC. BARTON, FLA.

STACK D.A.P. NO. 3 STATION R

Run No.	1	2	3
Date	12/16/71	12/18/71	12/20/71
Time Started	18:56	15:51	19:12
Time Ended	19:27	16:21	19:43
Barometric Pressure, "Hg	30	30	30
Stack Pressure, "Hg	29	29	29
Final Meter Reading Ft ³	10.4	14.05	16.9
Initial Meter Reading Ft ³	7.4	10.5	14.1
Meter Volume (meter cond. Ft ³)	3	3.55	2.8
Gas Volume Sampled, *Ft ³	2.8571	3.4426	2.6666
Meter Temperature °F	98	88	98
Stack Temperature °F	174	171	173
Average Gas Flow Rate, *Ft ³ /min	19812	19019	17540
Ammonia, mg	57.9	1267.9	257.4
Ammonia lbs/hr	52.99	924.48	223.45
Ammonia lb/ton NH ₃ fed	11.52	82.543	21.486
Ammonia gr/SCF	0.31006	5.635	1.4769
Ammonia gr/CF Stack Cond.	0.17837	3.2021	0.80901

* Dry, 70°F, 29.92 "Hg



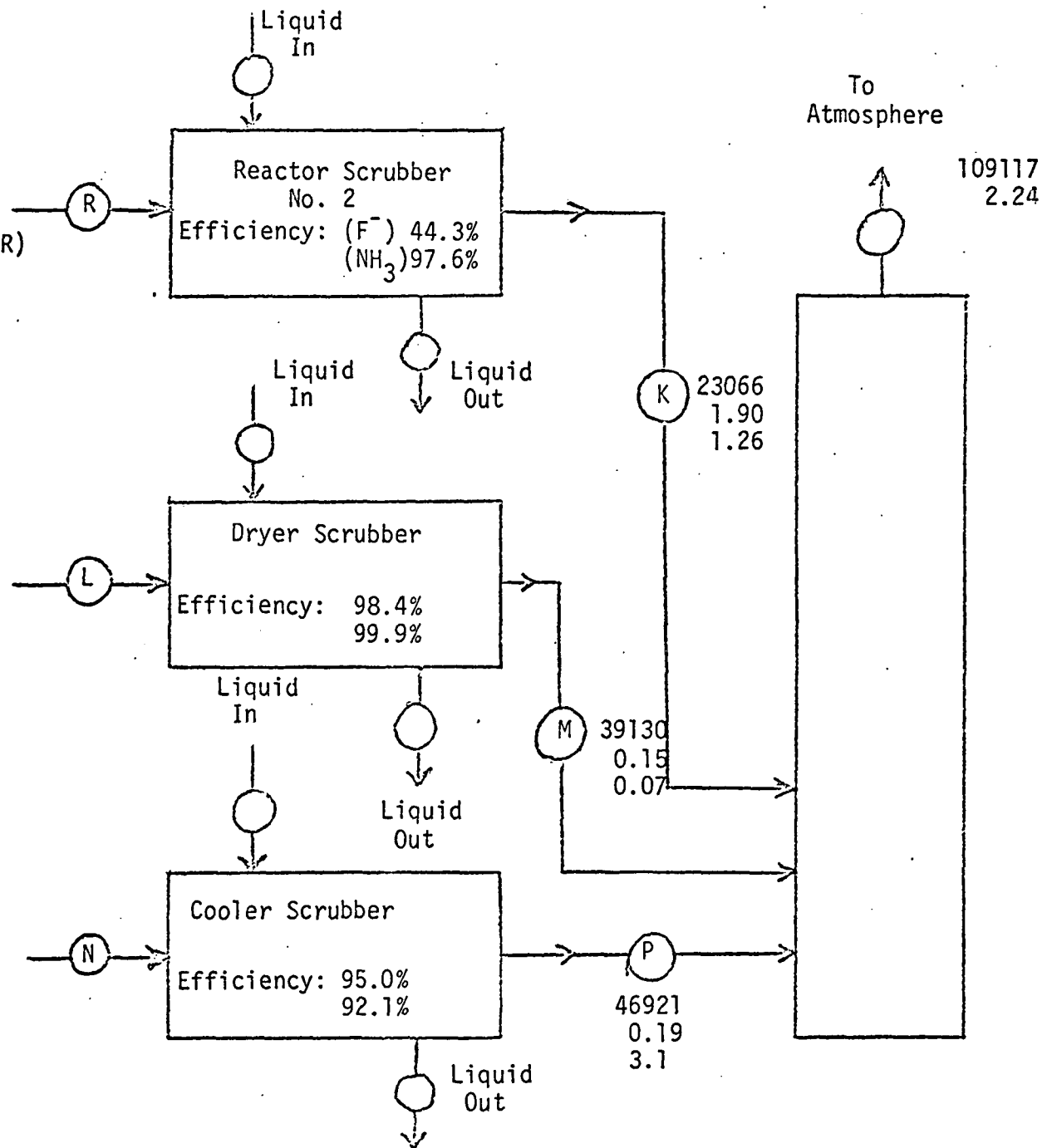
environmental engineering, inc.

SCRUBBER EFFICIENCY

Flow: 19812(DSCFM)
Total Fluoride: 3.41 (#/HR)
Ammonia: 53 (#/HR)

30655
9.29
252.6

36019
3.79
39.2



C. F. Chemicals
Diammonium Phosphate
Run 1

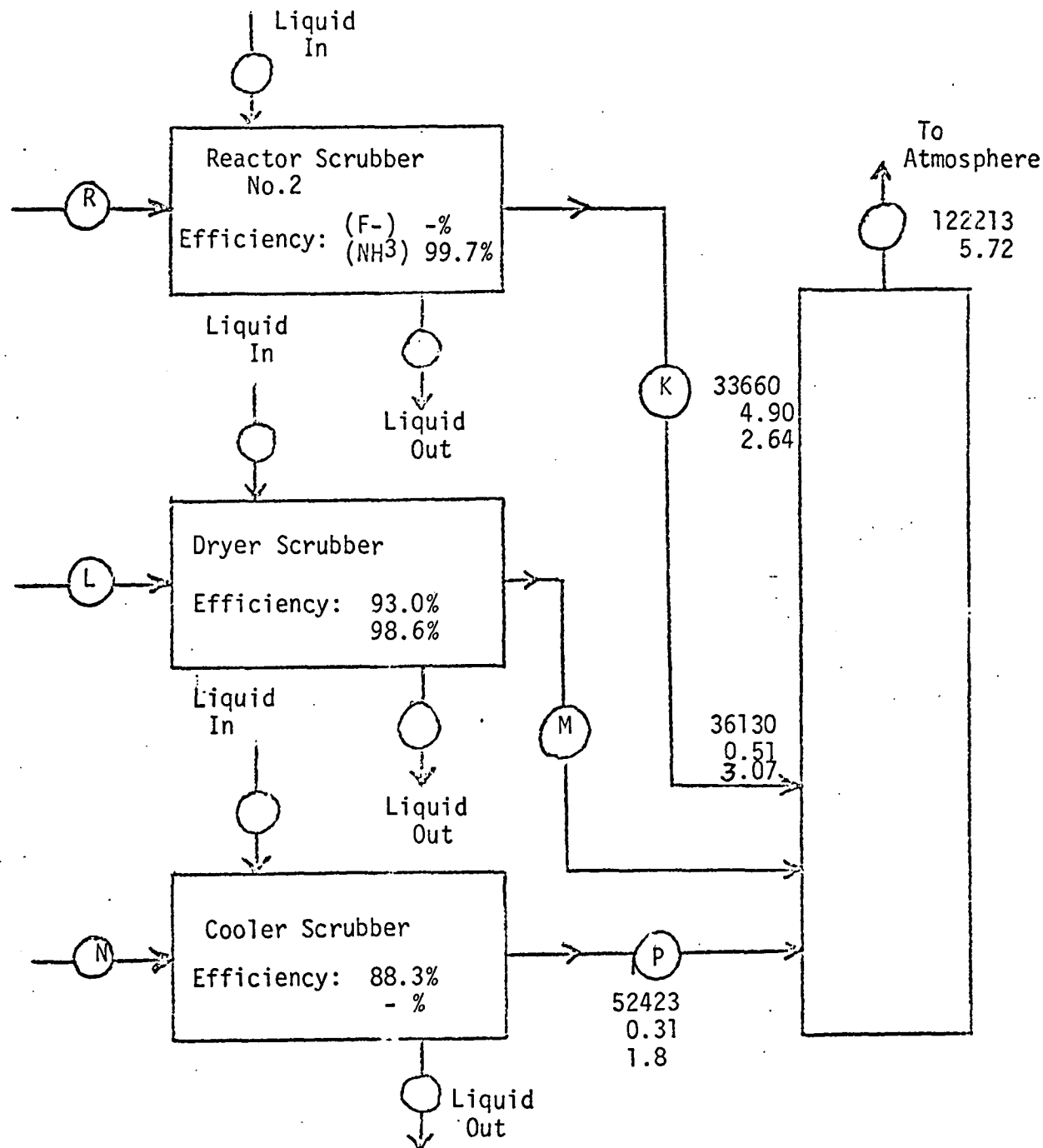
Flow: 19019 (DSCFM)

Total
Fluoride: 2.51 (#/HR)

Ammonia 924 (#/HR)

36625
7.25
216.7

34373
2.65
0.06



C. F. Chemicals
Diammonium Phosphate
Run 2

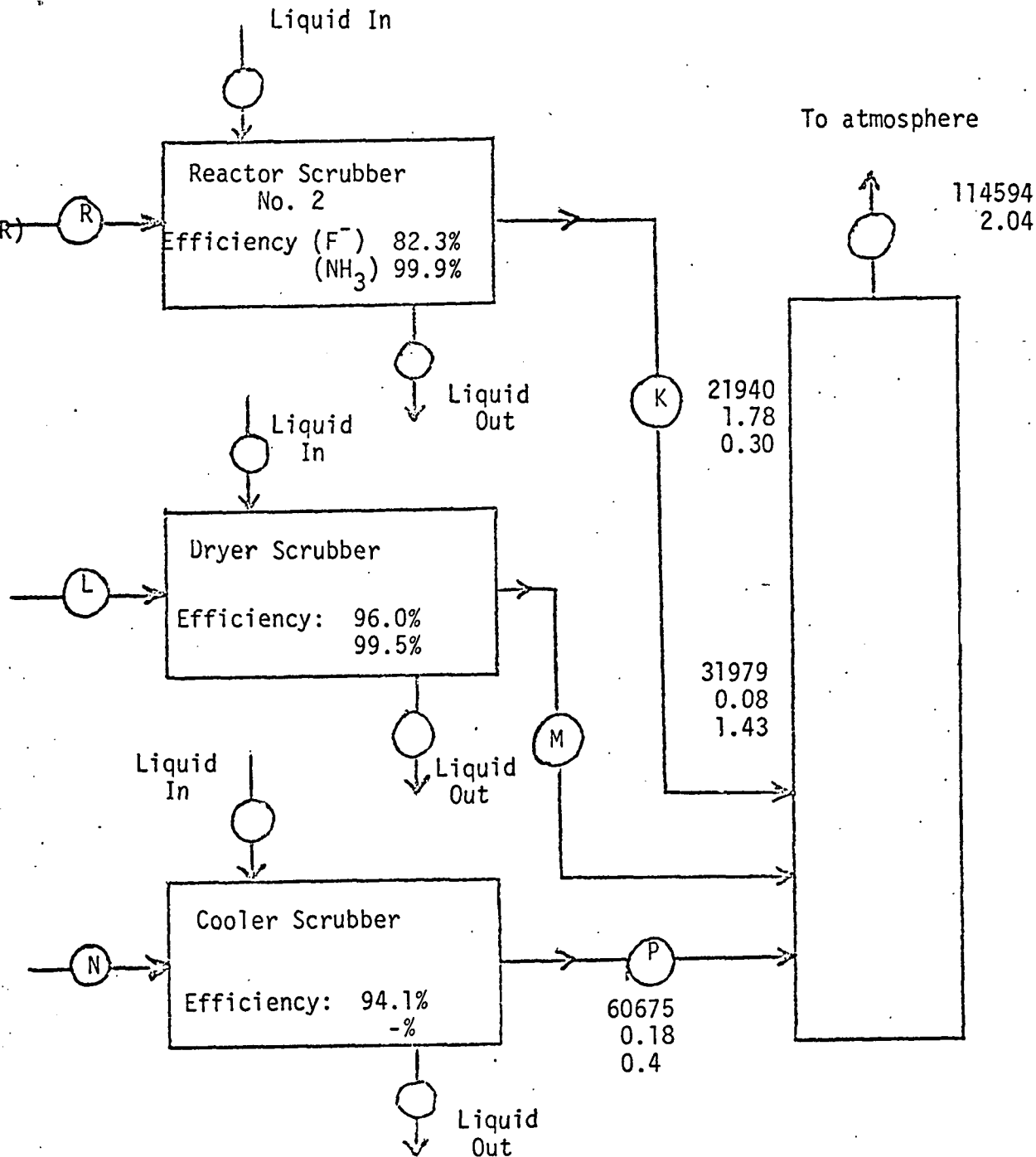
Flow: 17540 (DSCFM)

Total Fluoride: 10.03 (#/HR)

Ammonia: 223 #/HR

34855
1.98
267.4

41447
3.07
0.18



C.F. Chemicals
Diammonium Phosphate
Run 3

APPENDIX B

Field Data

PRELIMINARY MOISTURE DETERMINATION

PRELIMINARY CHECK FOR STACK GAS
MOISTURE CONTENT AND SPECIFIC GRAVITY

Plant C.F. Chemicals, Inc Stack DAP#3, Station "K"
Date 12-16-71 Sample Time 1145-1200 Barometric Pressure 30

Moisture Content -- Method 1

Final Dry Test Meter Reading 8.438 Ft³
Initial Dry Test Meter Reading 6.880 Ft³
Dry Test Meter Volume Sampled 1.558 Ft³
Average Meter Temperature 92 °F
Average Meter Vacuum — "Hg
Average Meter Orifice ΔH — "H₂O
Sampling Rate 2.9 LPM
Barometric Pressure @ Meter Orifice — "Hg
Dry Gas Volume Sampled @ 70 °F, 29.92 "Hg 1.500 Ft³
Condensate Volume 2 ml
Water Vapor Volume @ 70 °F, 29.92 "Hg 0.095 Ft³
Moisture Fraction, H₂O 0.08 Fraction Of Dry Air, FDA 0.92

Moisture Content -- Method 2

Dry Bulb Temp. _____ °F Wet Bulb Temp. _____ °F Dew Point Temp. _____ °F
Vapor Pressure Of H₂O @ DP _____ "Hg Stack Pressure _____ "Hg
Moisture Fraction, H₂O _____ Fraction Of Dry Air, FDA _____

Specific Gravity

Dry Molecular Weight, M_d = [0.44(%CO₂)] + [0.32(%O₂)] + [0.28(%N₂ + CO)] = _____
Molecular Weight @ Stack Conditions, M_s = [(M_d)x(FDA)] + [(18)x(H₂O)] = _____
Specific Gravity (Referred to air), G_s = (M_s) ÷ (28.99) = _____

PRELIMINARY CHECK FOR STACK GAS
MOISTURE CONTENT AND SPECIFIC GRAVITY

Plant C.F. Chemicals, Inc. Stack DAP#3, Station "L"
Date 12-16-71 Sample Time 1145 Barometric Pressure 30

Moisture Content -- Method 1

Final Dry Test Meter Reading 60.766 Ft³
Initial Dry Test Meter Reading 59.766 Ft³
Dry Test Meter Volume Sampled 1.000 Ft³
Average Meter Temperature 91 °F
Average Meter Vacuum — "Hg
Average Meter Orifice ΔH — "H₂O
Sampling Rate _____ LPM
Barometric Pressure @ Meter Orifice — "Hg
Dry Gas Volume Sampled @ 70 °F, 29.92 "Hg 0.964 Ft³
Condensate Volume 2.1 ml
Water Vapor Volume @ 70 °F, 29.92 "Hg 0.10 Ft³
Moisture Fraction, H₂O 0.12 Fraction Of Dry Air, FDA 0.88

Moisture Content -- Method 2

Dry Bulb Temp. 160 °F Wet Bulb Temp. 125 °F Dew Point Temp. 122 °F
Vapor Pressure Of H₂O @ DP 3.64 "Hg Stack Pressure 29.7 "Hg
Moisture Fraction, H₂O 0.12 Fraction Of Dry Air, FDA 0.88

Specific Gravity

Dry Molecular Weight, $M_d = [0.44(\%CO_2)] + [0.32(\%O_2)] + [0.28(\%N_2 + CO)] =$ _____
Molecular Weight @ Stack Conditions, $M_s = [(M_d) \times (FDA)] + [(18) \times (H_2O)] =$ _____
Specific Gravity (Referred to air), $G_s = (M_s) \div (28.99) =$ _____

PRELIMINARY CHECK FOR STACK GAS
MOISTURE CONTENT AND SPECIFIC GRAVITY

Plant C.F. Chemicals, Inc. Stack DAP # 3, Station "M"
Date 12-16-71 Sample Time 1220-1240 Barometric Pressure 30 "Hg

Moisture Content -- Method 1

Final Dry Test Meter Reading 939.600 Ft³
Initial Dry Test Meter Reading 935.700 Ft³
Dry Test Meter Volume Sampled 3.900 Ft³
Average Meter Temperature 82 °F
Average Meter Vacuum — "Hg
Average Meter Orifice ΔH 0.12 "H₂O
Sampling Rate 5.5 LPM
Barometric Pressure @ Meter Orifice 30 "Hg
Dry Gas Volume Sampled @ 70 °F, 29.92 "Hg 3.823 Ft³
Condensate Volume 10.6 ml
Water Vapor Volume @ 70 °F, 29.92 "Hg 0.502 Ft³
Moisture Fraction, H₂O 0.14 Fraction Of Dry Air, FDA 0.86

Moisture Content -- Method 2

Dry Bulb Temp. _____ °F Wet Bulb Temp. _____ °F Dew Point Temp. _____ °F
Vapor Pressure Of H₂O @ DP _____ "Hg Stack Pressure _____ "Hg
Moisture Fraction, H₂O _____ Fraction Of Dry Air, FDA _____

Specific Gravity

Dry Molecular Weight, $M_d = [0.44(\%CO_2)] + [0.32(\%CO_2)] + [0.28(\%N_2 + CO)] =$ _____
Molecular Weight @ Stack Conditions, $M_s = [(M_d) \times (FDA)] + [(18) \times (H_2O)] =$ _____
Specific Gravity (Referred to air), $G_s = (M_s) \div (28.99) =$ _____

PRELIMINARY CHECK FOR STACK GAS
MOISTURE CONTENT AND SPECIFIC GRAVITY

Plant C.F. Chemicals, Inc. Stack DAP #3, Station "N"
Date 12-16-71 Sample Time 1200-1215 Barometric Pressure 30 "Hg

Moisture Content -- Method 1

Final Dry Test Meter Reading 635.000 Ft³
Initial Dry Test Meter Reading 632.145 Ft³
Dry Test Meter Volume Sampled 2.855 Ft³
Average Meter Temperature 92 °F
Average Meter Vacuum — "Hg
Average Meter Orifice ΔH 0.05 "H₂O
Sampling Rate 5.4 LPM
Barometric Pressure @ Meter Orifice 30 "Hg
Dry Gas Volume Sampled @ 70 °F, 29.92 "Hg 2.748 Ft³
Condensate Volume 1.3 ml
Water Vapor Volume @ 70 °F, 29.92 "Hg 0.062 Ft³
Moisture Fraction, H₂O 0.05 Fraction Of Dry Air, FDA 0.95

Moisture Content -- Method 2

Dry Bulb Temp. 140 °F Wet Bulb Temp. 100 °F Dew Point Temp. 92 °F
Vapor Pressure Of H₂O @ DP 1.51 "Hg Stack Pressure 29.7 "Hg
Moisture Fraction, H₂O 0.05 Fraction Of Dry Air, FDA 0.95

Specific Gravity

Dry Molecular Weight, $M_d = [0.44(\%CO_2)] + [0.32(\%O_2)] + [0.28(\%N_2 + CO)] =$ _____
Molecular Weight @ Stack Conditions, $M_s = [(M_d) \times (FDA)] + [(18) \times (H_2O)] =$ _____
Specific Gravity (Referred to air), $G_s = (M_s) \div (28.99) =$ _____

PRELIMINARY CHECK FOR STACK GAS
MOISTURE CONTENT AND SPECIFIC GRAVITY

Plant C.F. Chemicals, Inc. Stack DAP#3, Station "P"
Date 12-16-71 Sample Time 1150-1200 Barometric Pressure 30 "Hg

Moisture Content -- Method 1

Final Dry Test Meter Reading 391.456 Ft³
Initial Dry Test Meter Reading 390.456 Ft³
Dry Test Meter Volume Sampled 1.000 Ft³
Average Meter Temperature 90 °F
Average Meter Vacuum — "Hg
Average Meter Orifice ΔH — "H₂O
Sampling Rate 2.8 LPM
Barometric Pressure @ Meter Orifice — "Hg
Dry Gas Volume Sampled @ 70 °F, 29.92 "Hg 0.966 Ft³
Condensate Volume 2.5 ml
Water Vapor Volume @ 70 °F, 29.92 "Hg 0.119 Ft³
Moisture Fraction, H₂O 0.13 Fraction Of Dry Air, FDA 0.87

Moisture Content -- Method 2

Dry Bulb Temp. _____ °F Wet Bulb Temp. _____ °F Dew Point Temp. _____ °F
Vapor Pressure Of H₂O @ DP _____ "Hg Stack Pressure _____ "Hg
Moisture Fraction, H₂O _____ Fraction Of Dry Air, FDA _____

Specific Gravity

Dry Molecular Weight, $M_d = [0.44(\%CO_2)] + [0.32(\%O_2)] + [0.28(\%N_2 + CO)] =$ _____
Molecular Weight @ Stack Conditions, $M_s = [(M_d) \times (FDA)] + [(18) \times (H_2O)] =$ _____
Specific Gravity (Referred to air), $G_s = (M_s) \div (28.99) =$ _____

PRELIMINARY CHECK FOR STACK GAS
MOISTURE CONTENT AND SPECIFIC GRAVITY

Plant C.F. Chemicals, Inc. Stack DAP #3, Station "R"
Date 12-16-71 Sample Time 1145-1202 Barometric Pressure 30 "Hg

Moisture Content -- Method 1

Final Dry Test Meter Reading 096.500 Ft³
Initial Dry Test Meter Reading 094.000 Ft³
Dry Test Meter Volume Sampled 2.500 Ft³
Average Meter Temperature 90 °F
Average Meter Vacuum — "Hg
Average Meter Orifice ΔH 0.05 "H₂O
Sampling Rate 4.2 LPM
Barometric Pressure @ Meter Orifice 30 "Hg
Dry Gas Volume Sampled @ 70 °F, 29.92 "Hg 2.415 Ft³
Condensate Volume 2 ml
Water Vapor Volume @ 70 °F, 29.92 "Hg 0.095 Ft³
Moisture Fraction, H₂O 0.06 Fraction Of Dry Air, FDA 0.94

Moisture Content -- Method 2 (12-20-71)

Dry Bulb Temp. 169 °F Wet Bulb Temp. 165 °F Dew Point Temp. 164.5 °F
Vapor Pressure Of H₂O @ DP 10.8 "Hg Stack Pressure 29 "Hg
Moisture Fraction, H₂O 0.37 Fraction Of Dry Air, FDA 0.63

Specific Gravity

Dry Molecular Weight, $M_d = [0.44(\%CO_2)] + [0.32(\%O_2)] + [0.28(\%N_2 + CO)] =$ _____
Molecular Weight @ Stack Conditions, $M_s = [(M_d) \times (FDA)] + [(18) \times (H_2O)] =$ _____
Specific Gravity (Referred to air), $G_s = (M_s) \div (28.99) =$ _____

FLUORIDE EMISSIONS

SOURCE SAMPLING FIELD DATA SHEET

Plant C.F. Chemicals (Dap)Sampling Location K outlet Reactor Sander #2 Sketch of StackDate 12/16/71 Run No. 1Time Start 16:00 Time End 6.20Sampling Time/Point 10 @ 12 minDB 170 °F, WB _____ °F, VF @ DP _____ "HgMoisture 8 %, FDA 0.92 Gas Density Factor _____Barometric Press 30 "Hg, Stack Press 29 "HgWeather HOT

Temp. _____ °F, W/D _____, W/S _____

Sample Box No. _____ Meter Box No. 5Meter AH 1.68 Pitot Corr. Factor 0.82Nozzle Dia. 1/4 in., Probe Length 8 ft

Probe Heater Setting _____

Stack Dimensions: Inside Diameter 42 inInside Area 9.61 ft²

Height _____ ft

Mat'l Processing Rate _____

Final Gas Meter Reading 452.379 ft³Initial Gas Meter Reading 343.918 ft³Total Condensate in Impingers 605 mlMoisture in Silica Gel 229.8 - 192.5 = 37.3 gmSilica Gel Container No. 208 Filter No. 72-023Orsat: CO₂ 0O₂ 19.4CO 0N₂ _____

Excess _____

Air _____

Test Conducted By: G. AllenB. DemeryT. Arrorb

Remarks: _____

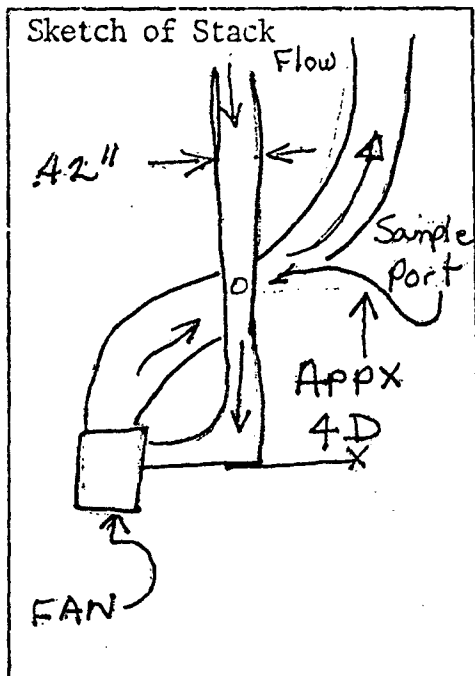
Port and Traverse Point No.	Distance from End of Port (in)	Clock Time	Gas Meter Reading (ft ³)	Stack Velocity Head ("H ₂ O)	Meter Orifice Press. Diff. ("H ₂ O)		Stack Gas Temp. (°F)	Gas Sample Temp. & Dry Gas Meter (°F)		Sample Box Temp. (°F)	Last Impinger Temp. (°F)	Vacuum on Sample Train ("Hg)
					Calc.	Actual		In	Out			
17 1	2 7/8	4.20	343.918	0.54	1.7	1.7	160	99	100	0	90	7.1
			353.700		1.65	1.65	165	97	100	6	79	7.9
2	1/8		357.85	0.41	1.39	1.39	165	97	99	12	86	6.8
			362.85		1.29	1.29	162	97	99	3	89	6.1
3			366.58	0.40	1.26	1.26	162	97	99	9	85	6.1
			370.96		1.35	1.35	162	96	99	15	84	6.2
* 4			377.1	0.55	1.67	1.67	160	96	99	6	82	7.5
			384.5		—	4.3	150	96	98	12	83	22.5
5			391.8	4.5	—	4.3	165	96	98	3	88	23

* V. Head Jumped from .55 to 3.5 at this point

[illegible]

** V. Head Back to Normal

Plant C. F. Chemical
 Sampling Location Outlet Reactor Scrubber
 Date 12/18/71 Run No. Station K
 Time Start 1345 Time End 1543
 Sampling Time/Point 6 mins. - 120 Total
 DB — °F, WB — °F, VF @ DP — "Hg
 Moisture 22%, FEA 68, Gas Density Factor —
 Barometric Press 30 "Hg, Stack Press 29 "Hg
 Weather Partly Cloudy - Fair
 Temp. 75 °F, W/D S, W/S 5-10
 Sample Box No. 5 Meter Box No. 5
 Meter Al 1.68 Pitot Corr. Factor 0.82
 Nozzle Dia. .25 in., Probe Length 8 ft
 Probe Heater Setting —
 Stack Dimensions: Inside Diameter 42 in
 Inside Area — ft²
 Height — ft



Mat'l Processing Rate

Final Gas Meter Reading 596.322 ft³Initial Gas Meter Reading 462.268 ft³Total Condensate in Impingers 940 mlMoisture in Silica Gel 97.1 gmSilica Gel Container No. AP-III Filter No. 72-020Orsat: CO₂ 0O₂ 21CO 0N₂ —Excess Air —Test Conducted By: AllenARROYODEMERYRemarks: —

Port and Traverse Point No.	Distance from End of Port (in)	Clock Time	Gas Meter Reading (ft ³)	Stack Velocity Head ("H ₂ O)	Meter Orifice Press. Diff. ("H ₂ O)		Stack Gas Temp. (°F)	Gas Sample Temp. @ Dry Gas Meter (°F)		Sample Box Temp. (°F) *	Last Impinger Temp. (°F)	Vacuum on Sample Train ("Hg)
					Calc.	Actual		In	Out			
1		13.45	468.8	1.00	2.5	2.5	170	72	72	0	72	8.9
		13.51	473.55	0.95	2.4	2.4	170	72	73	6	71	8.2
2		13.57	479.16	0.99	2.45	2.45	170	72	73	12	71	9.1
		14.03	484.87	1.0	2.5	2.5	170	72	73	3	73	9.1
3		14.09	490.78	1.15	2.85	2.85	160	72	73	9	76	11.5
		14.15	497.65	1.7	3.25	3.9	170	73	73	15	85	22.2
4		14.21	504.66	2.2	5.5	3.7	170	79	75	6	85	22.6
		14.27	512.11	2.3	5.8	4.1	170	81	76	12	80	22.6
5		14.33	519.31	2.9	7.2	4.1	170	79	78	3	67	22.6

~~Sample
Box
Temp.
(°F)~~

dia

* STOPPED TO EMPTY WATER IN FILTER + 3rd IMPRINGER

SOURCE SAMPLING FIELD DATA SHEET

Plant C.F. Chemicals DAP
 Sampling Location Outlet Reactor Scrubber
 Date 12/20/71 Run No. 3
 Time Start 6:00 Time End 8:00
 Sampling Time/Point 6 min.
 DB — °F, WB — °F, VF @ DP — "Hg
 Moisture 22%, FDA —, Gas Density Factor —
 Barometric Press 30 "Hg, Stack Press 29 Hg
 Weather Night
 Temp. — °F, W/D —, W/S —
 Sample Box No. — Meter Box No. 5
 Meter 4110 6.68 Pitot Corr. Factor 0.82
 Nozzle Dia. 0.25 in., Probe Length 8 ft
 Probe Heater Setting —
 Stack Dimensions: Inside Diameter 42 in
 Inside Area — ft²
 Height — ft

Sketch of Stack
#2

Mat'l Processing Rate —Final Gas Meter Reading 700.805 ft³Initial Gas Meter Reading 596.472 ft³Total Condensate in Impingers 640 mlMoisture in Silica Gel 231-200.5=30.5 gmSilica Gel Container No. 212 Filter No. 72-633

Orsat:	CO ₂	<u>0</u>			
	O ₂	<u>20.6</u>			
	CO	<u>0</u>			
	N ₂	<u>79.4</u>			

Excess
Air

Test Conducted By: G. Allen
B. Demery

Remarks: —
—
—

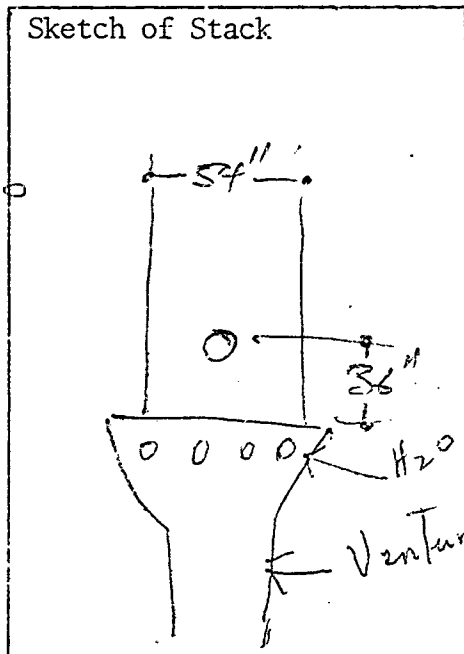
Port and Traverse Point No.	Distance from End of Port (in)	Clock Time	Gas Meter Reading (ft ³)	Stack Velocity Head ("H ₂ O)	Meter Orifice Press. Diff. ("H ₂ O)		Stack Gas Temp. (°F)	Gas Sample Temp. & Dry Gas Meter (°F)		Sample Box Temp. (°F)	Last Impinger Temp. (°F)	Vacuum on Sample Train ("Hg)
					Calc.	Actual		In	Out			
1-1	Same as run #1	6:00	596.472									
			600.0	0.33	0.89	0.89	170	86	87	0	70	4.1
			603.4	0.34	0.87	0.87	170	87	82	6	67	4.0
2			606.6	0.33	0.90	0.90	170	85	77	12	69	4.1
			610.4	0.34	0.95	0.95	170	84	75	3	69	4.1
3			613.9	0.34	0.95	0.95	170	83	74	9	70	4.2
			617.8	0.47	1.20	1.20	170	81	74	15	70	5.0
4			622.4	0.68	1.20	1.20	170	80	75	6	70	5.2
			627.1	0.72	1.80	1.80	170	79	76	12	70	7.2
5			632.6	1.1	2.70	2.70	170	79	78	3	70	12.2

[illegible]

SOURCE SAMPLING FIELD DATA SHEET

Plant CF Chemicals
 Sampling Location See L (Change)
 Date 12/16/71 Run No. 1
 Time Start 4:20 Time End _____
 Sampling Time/Point 7.5 min @ 120
 DB 160 °F, WB 125 °F, VF @ DP _____ "Hg
 Moisture 9.28%, FDA 81.7%, Gas Density Factor _____
 Barometric Press 30 "Hg, Stack Press 30 "Hg
 Weather clear
 Temp. _____ °F, W/D _____, W/S _____
 Sample Box No. _____ Meter Box No. _____
 Meter ΔH@ 1.6 Pitot Corr. Factor .82
 Nozzle Dia. 1/4 in., Probe Length 8 ft
 Probe Heater Setting 55%
 Stack Dimensions: Inside Diameter 54 in
 Inside Area _____ ft²
 Height _____ ft

Sketch of Stack



Mat'l Processing Rate _____

Final Gas Meter Reading 154.949 ft³
 Initial Gas Meter Reading 60.895 ft³
 Total Condensate in Impingers 410 ml 435.6
 Moisture in Silica Gel 25.6 gm
 Silica Gel Container No. 2 Filter No. 72015

Orsat: CO₂ _____
 O₂ 20.4
 CO _____
 N₂ _____
 Excess Air _____

Test Conducted By: John Tucker
Eric Johnson

Remarks: _____

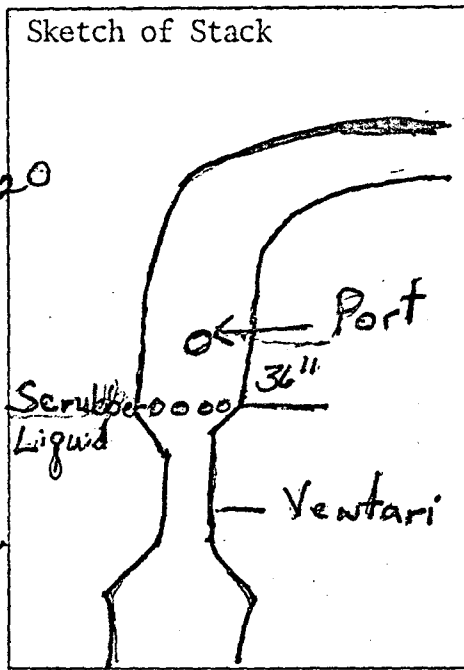
Port and Traverse Point No.	Distance from End of Port (in)	Clock Time	Gas Meter Reading (ft ³)	Stack Velocity Head ("H ₂ O)	Meter Orifice Press. Diff. ("H ₂ O)		Stack Gas Temp. (°F)	Gas Sample Temp. @ Dry Gas Meter (°F)		Sample Box Temp. (°F)	Last Impinger Temp. (°F)	Vacuum on Sample Train ("Hg)
					Calc.	Actual		In	Out			
1	2 3/8	4:23	60.895	0.35	1.10	1.10	160	104	100	-	85	5.0
2	4	4:30	70.2	0.38	1.2	1.2	160	112	100	-	85	6.0
3	5 7/8	4:36	75.2	0.45	1.4	1.4	160	120	100	-	85	6.0
4	7 7/8	4:45	80.3	0.47	1.55	1.55	160	124	104	-	85	6.0
5	10 1/8	4:52	85.4	0.44	1.70	1.40	162	126	110	-	85	6.5
6	12 3/4	5:00	90.7	0.46	1.40	1.40	162	131	114	-	85	6.5
7	16	5:08	96.0	0.46	1.40	1.60	162	131	116	-	90	6.5
8	20 5/8	5:16	101.3	0.46	1.40	1.40	162	142	120	-	84	6.5
9	33 3/8	5:23	106.7	0.53	1.70	1.70	161	145	123	-	82	7.5

[illegible]

* head increase during last 2 min. of post
* ~~last~~ ~~last~~ ~~last~~ first 2 min. of post

SOURCE SAMPLING FIELD DATA SHEET

Plant FC Chemicals
 Sampling Location Point L
 Date 12/15/71 Run No. 2
 Time Start 1:50 Time End 3:50
 Sampling Time/Point 7.5 min/Point 120
 DB °F, WB °F, VF @ DP "Hg
 Moisture 120%, FDA 82 Gas Density Factor +
 Barometric Press 30 "Hg, Stack Press 30 "Hg
 Weather Overcast
 Temp. °F, W/D , W/S
 Sample Box No. Meter Box No.
 Meter 4H @ 0.160 Pitot Corr. Factor 0.82
 Nozzle Dia. 0.25 in., Probe Length 8 ft
 Probe Heater Setting 60%
 Stack Dimensions: Inside Diameter 54 in
 Inside Area ft²
 Height ft



Mat'l Processing Rate
 Final Gas Meter Reading 254.540 ft³
 Initial Gas Meter Reading 160.558 ft³
 Total Condensate in Impingers 191 ml
 Moisture in Silica Gel 24.9 gm
 Silica Gel Container No. 215 Filter No. 72019
 Orsat: CO₂
 O₂ 20.5
 CO
 N₂
 Excess Air
 Test Conducted By: T. Tucker
 Andy Taylor

Remarks:

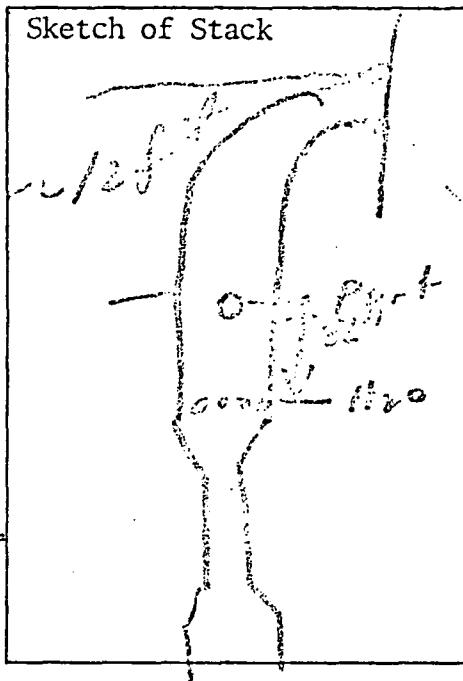
Port and Traverse Point No.	Distance from End of Port (in)	Clock Time	Gas Meter Reading (ft ³)	Stack Velocity Head ("H ₂ O)	Meter Orifice Press. Diff. ("H ₂ O)		Stack Gas Temp. (°F)	Gas Sample Temp. @ Dry Gas Meter (°F)		Sample Box Temp. (°F)	Last Impinger Temp. (°F)	Vacuum on Sample Train ("Hg)
					Calc.	Actual		In	Out			
1	2 3/8	1:57	166.400	0.38	1.0	1.0	150	80	72		62	4.5
2	4	2:05	171.100	0.45	1.45	1.15	150	85	73		75	5.5
3	5 1/8	2:13	175.8	0.48	1.15	1.15	150	96	78		86	6.0
4	7 7/8	2:20	180.4	0.45	1.15	1.15	148	102	82		80	6.0
5	10 7/8	2:28	185.4	0.45	1.15	1.15	149	110	86		75	5.5
6	12 3/4	2:35	190.1	0.45	1.15	1.15	149	112	90		72	6.0
7	16	2:42	194.9	0.43	1.14	1.14	149	118	95		78	5.5
8	20 5/8	2:50	200.2	0.43	1.14	1.14	149	118	98		70	5.5
9	33 3/8	2:57	204.8	0.43	1.14	1.14	149	120	100		68	5.5

[illegible]

SOURCE SAMPLING FIELD DATA SHEET

Plant C F Chemicals
 Sampling Location 7" 2"
 Date 12/29/71 Run No. 3
 Time Start 1805 Time End 20:05
 Sampling Time/Point 7.5/16 = 120
 DB °F, WB °F, VF & DP "Hg
 Moisture 18 %, FDA 82 Gas Density Factor
 Barometric Press 30 "Hg, Stack Press 30 "Hg
 Weather Clear
 Temp. °F, W/D , W/S
 Sample Box No. Meter Box No.
 Meter 4H2 1.60 Pitot Corr. Factor 0.82
 Nozzle Dia. 0.25 in., Probe Length 8 ft
 Probe Heater Setting 60%
 Stack Dimensions: Inside Diameter 34 in
 Inside Area ft²
 Height ft

Sketch of Stack

Mat'l Processing Rate Final Gas Meter Reading 348.330 ft³Initial Gas Meter Reading 260.233 ft³Total Condensate in Impingers (349.200 - 149.200) = 200.0 gmMoisture in Silica Gel 211.1 - 190 = 21.1 gmSilica Gel Container No. 223 Filter No. 72031

Orsat: CO₂
 O₂
 CO
 N₂
 Excess Air

Test Conducted By: T. Taylor
Andy TaylorRemarks:

Port and Traverse Point No.	Distance from End of Port (in)	Clock Time	Gas Meter Reading (ft ³)	Stack Velocity Head ("H ₂ O)	Meter Orifice Press. Diff. ("H ₂ O)		Stack Gas Temp. (°F)	Gas Sample Temp. & Dry Gas Meter (°F)		Sample Box Temp. (°F)	Last Impinger Temp. (°F)	Vacuum on Sample Train ("Hg)
					Calc.	Actual		In	Out			
		<u>6:03</u>	<u>260.233</u>									
<u>1</u>	<u>2 3/8</u>	<u>6:10</u>	<u>265.400</u>	<u>0.60</u>	<u>1.6</u>	<u>1.6</u>	<u>150</u>	<u>90</u>	<u>83</u>		<u>64</u>	<u>5.0</u>
<u>2</u>	<u>4</u>	<u>6:18</u>	<u>270.6 *</u>	<u>0.58</u>	<u>1.4</u>	<u>1.4</u>	<u>150</u>	<u>98</u>	<u>85</u>		<u>66</u>	<u>5.0</u>
<u>3</u>	<u>5 1/8</u>	<u>6:25</u>	<u>276.3</u>	<u>0.5/0.52</u>	<u>1.4/2.2</u>	<u>1.4/2.2</u>	<u>150</u>	<u>106</u>	<u>83</u>		<u>68</u>	<u>6.0</u>
<u>4</u>	<u>7 1/8</u>	<u>6:33</u>	<u>282.0</u>	<u>0.55</u>	<u>1.5</u>	<u>1.5</u>	<u>150</u>	<u>112</u>	<u>92</u>		<u>70</u>	<u>6.0</u>
<u>5</u>	<u>10 1/8</u>	<u>6:40</u>	<u>286.1</u>	<u>0.55</u>	<u>1.5</u>	<u>1.5</u>	<u>150</u>	<u>112</u>	<u>95</u>		<u>70</u>	<u>20.0</u>
<u>6</u>	<u>12 3/4</u>	<u>6:48</u>	<u>292.0</u>	<u>0.55</u>	<u>1.5</u>	<u>1.5</u>	<u>150</u>	<u>114</u>	<u>96</u>		<u>70</u>	<u>20.0</u>
<u>7</u>	<u>16</u>	<u>7:05</u>	<u>297.0</u>	<u>0.50</u>	<u>1.4</u>	<u>1.4</u>	<u>151</u>	<u>118</u>	<u>102</u>		<u>72</u>	<u>5.0</u>
<u>8</u>	<u>20 1/8</u>	<u>7:12</u>	<u>302.3</u>	<u>0.45</u>	<u>1.25</u>	<u>1.25</u>	<u>151</u>	<u>122</u>	<u>108</u>		<u>74</u>	<u>5.0</u>
<u>9</u>	<u>33 1/8</u>	<u>7:20</u>	<u>307.0</u>	<u>0.48</u>	<u>1.25</u>	<u>1.25</u>	<u>152</u>	<u>126</u>	<u>110</u>		<u>76</u>	<u>5.0</u>

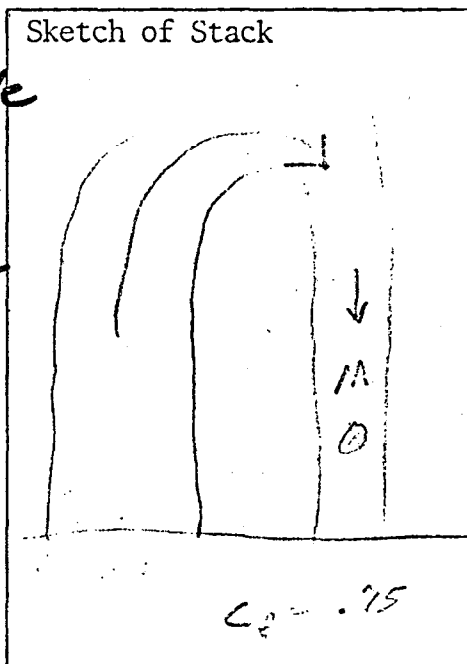
* 23 min into run - Velocity change -
 then a change back to 0.50

[illegible]

SOURCE SAMPLING FIELD DATA SHEET

Plant CF CHEMICALS
 Sampling Location Scrubber "M"
 Date 12/16/71 Run No. 4 Fluoride
 Time Start 5:50 Time End 7:12
 Sampling Time/Point 6 min 102
 DB 126 °F, WB _____ °F, VF @ DP _____ "Hg
 Moisture 137%, FDA 86%, Gas Density Factor .95
 Barometric Press 30 "Hg, Stack Press 28.1 "Hg
 Weather Beautiful / SB AT Beach
 Temp. _____ °F, W/D _____, W/S _____
 Sample Box No. 4 Meter Box No. _____
 Meter 1.62 Pitot Corr. Factor .84
 Nozzle Dia. .25 in., Probe Length _____ ft
 Probe Heater Setting 40%
 Stack Dimensions: Inside Diameter 56 in
 Inside Area _____ ft²
 Height _____ ft

Sketch of Stack



FILTER # 72013

6" nipple protruding / Actual time is plus 30 min
start 5:30 END 7:12

Mat'l Processing Rate 1031.582
 Final Gas Meter Reading _____ ft³
 Initial Gas Meter Reading 948.200 ft³
 Total Condensate in Impingers 225 Total ml
 Moisture in Silica Gel 5.2 gm
 Silica Gel Container No. 214 Filter No. NONE
 Orsat: CO₂ 0.6%
 O₂ 19.8%
 CO 0%
 BAL ⇒ N₂ 79.6
 Excess Air _____
 Test Conducted By: J. Chadbourne
M. Jackson

Remarks: _____

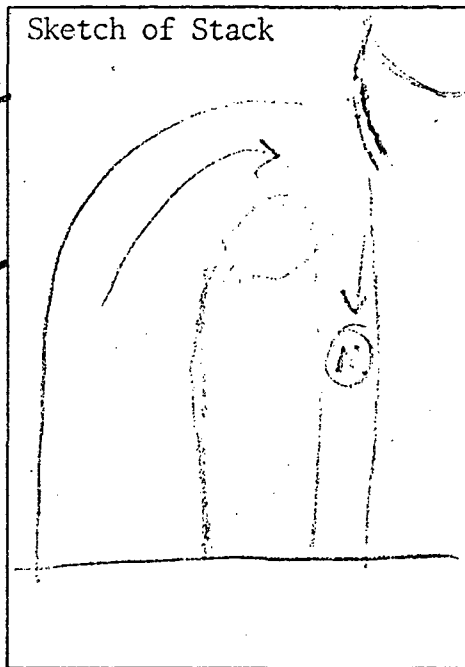
Port and Traverse Point No.	Distance from End of Port (in)	Clock Time	Gas Meter Reading (ft ³)	Stack Velocity Head ("H ₂ O)	Meter Orifice Press. Diff. ("H ₂ O)		Stack Gas Temp. (°F)	Gas Sample Temp. @ Dry Gas Meter (°F)		Sample Box Temp. (°F)	Last Impinger Temp. (°F)	Vacuum on Sample Train ("Hg)
					Calc.	Actual		In	Out			
1.1	8	6:42	31.582 (std)									
3.5	8											
6.0	19 3/8											
8.7	10 7/8											
11.6	12 1/2	6:36	28.7	0.12	0.35	0.35		91	92		90	4
14.6	14 1/4	6:30	24.9	0.47	1.35	1.35		91	92		90	8
18.0	16 1/8	6:24	20.1	0.52	1.5	1.5	132	91	92		87	8
21.8	18 1/4	6:18	15.8	0.57	1.6	1.6		91	92		89	8
26.1	20 5/8	6:12	—	0.54	1.52	1.5		91	92		84	8

[illegible]

SOURCE SAMPLING FIELD DATA SHEET

ant **C F CHEMICALS**
 umpling Location **Scrubber #1**
 te **12/18/71** Run No. **2 F/verde**
 me Start **1:45** Time End **3:33**
 umpling Time/Point **6 MIN 102**
130 °F, WB **128** °F, VF @ DP "Hg
 isture **15** %, FDA **85** Gas Density Factor **.95**
 arometric Press **30** "Hg, Stack Press **28.1** "Hg
 eather **Fair**
 mp. **75** °F, W/D **5**, W/S **5 mph**
 ample Box No. **4** Meter Box No. _____
 eter **1.62** Pitot Corr. Factor _____
 zzle Dia. **.25** in., Probe Length _____ ft
 robe Heater Setting _____
 ack Dimensions: Inside Diameter **56** in
 Inside Area _____ ft²
 Height _____ ft

Sketch of Stack



6g = .72 75° Tm

6" Nipple protruding

Mat'l Processing Rate _____

Final Gas Meter Reading **133.072** ft³Initial Gas Meter Reading **52.34** ft³

Total Condensate in Impingers _____ ml

Moisture in Silica Gel **2065-1935 = 130** gmSilica Gel Container No. **205** Filter No. _____Orsat: CO₂ **0**O₂ **20.0**CO **0**Bal N₂ **80.0**

Excess Air _____

Test Conducted By: **J. Chadbourne**
M. Jackson

Remarks: _____

Port and Reverse Point No.	Distance from End of Port (in)	Clock Time	Gas Meter Reading (ft ³)	Stack Velocity Head ("H ₂ O)	Meter Orifice Press. Diff. ("H ₂ O)		Stack Gas Temp. (°F)	Gas Sample Temp. @ Dry Gas Meter (°F)		Sample Box Temp. (°F)	Last Impinger Temp. (°F)	Vacuum on Sample Train ("Hg)
					Calc.	Actual		In	Out			
	6 5/8				[2 Negative points]							
Neg	8											
Neg	9 3/8	3:33	133.072	Final Vol								
	10 7/8	3:27	132.40	.03	.07	.07	111	80	80	69	0	
	12 1/2	3:21	129.10	.275	.735	.735	111	-80	80	69	2	
	14 1/4	3:15	124.60	.59	1.60	1.60	111	81	78	69	3	
	16 1/8	3:09	120.06	.60	1.60	1.60	111	-81	77	69	3	
	18 1/4	3:03	114.6	.625	1.70	1.70	111	81	77	69	3	
	20 5/8	2:57	110.8	.675	1.82	1.82	111	80	77	69	4	

Port and Traverse Point No.	Distance from End of Port (in)	Clock Time	Gas Meter Reading (ft ³)	Stack Velocity Head ("H ₂ O)	Meter Orifice Press. Diff. ("H ₂ O)		Stack Gas Temp. (°F)	Gas Sample Temp. @ Dry Gas Meter (°F)		Sample Box Temp. (°F)	Last Impinger Temp. (°F)	Vacuum on Sample Train ("Hg)
					Cal.	Actual		In	Out			
	23 7/8	2:51	106.45	.52	1.4	1.4	111	79	77		68	3
	28	2:45	103.32	.28	.75	.75	111	78	76		68	1
	40	2:39	103.45	.24	.65	.65	111	77	75		67	1
	44 3/8	2:33	96.45	.46	1.25	1.25	111	77	75		67	3
	47 7/8	2:27	91.95	.63	1.7	1.7	111	77	74		67	3
	49 3/4	2:21	86.45	.83	2.25	2.25	111	76	74		68	4
	51 7/8	2:15	81.3	0.81	2.2	2.2	111	75	74		68	4
	53 3/4	2:09	76.0	0.90	2.4	2.4	111	74	75		67	4
	55 1/2	2:03	70.6	0.98	2.7	2.7	111	74	76		68	5
	57 1/8	1:57	64.5	1.20	3.25	3.25	111	74	76		67	6.5
	58 7/8	1:51		1.25	3.4	3.4	111	74	76		66	7
	60	1:45	52.34	1.15	3.0	3.0	111	74	76		59	4
			NH ₃ Sample									
		4:00	97.4						76			4.0
		4:08	98.2						76			4.0
		4:15	99.02						76			4.0
		4:22	99.71						73			4.0
		4:30	100.53						76			4.0

Plant CF CHEMICALS
 Sampling Location Scrubber "M"
 Date 12/22/71 Run No. 3 Fluoride
 Time Start 1800 Time End 1936
 Sampling Time/Point 6 MIN 96
 DB 114 °F, WB 112 °F, VF @ DP _____ "Hg
 Moisture 9.7%, FD 90.3 Gas Density Factor .95
 Barometric Press 30 "Hg, Stack Press 28.2 "Hg
 Weather FAIR
 Temp. 80 °F, W/D _____, W/S _____
 Sample Box No. 4 Meter Box No. _____
 Meter 411 1.62 Pitot Corr. Factor .84
 Nozzle Dia. .25 in., Probe Length _____ ft
 Probe Heater Setting _____
 Stack Dimensions: Inside Diameter 56 in
 Inside Area _____ ft²
 Height _____ ft

6" nipple protruding

Sketch of Stack

$\cdot 3 > .92$

$C_g = .75$ $.94$ $\frac{P_s}{P_a}$
 $24.2'' H_2O$ $\uparrow$
 $vac inst \approx 1.8'' Hg$

Mat'l Processing Rate

Final Gas Meter Reading 210.340 ft³

Initial Gas Meter Reading 134.915 ft³

Total Condensate in Impingers 242.0 ml

Moisture in Silica Gel 20.0 gm

Silica Gel Container No. 206 Filter No. _____

Orsat: CO₂ 0

O₂ 20.3

CO 0

N₂ _____

Excess

Air

Test Conducted By: J. Chadbourne
M. Jackson

Remarks: _____

Port and Traverse Point No.	Distance from End of Port (in)	Clock Time	Gas Meter Reading (ft ³)	Stack Velocity Head ("H ₂ O)	Meter Orifice Press. Diff. ("H ₂ O)		Stack Gas Temp. (°F)	Gas Sample Temp. & Dry Gas Meter (°F)		Sample Box Temp. (°F)	Last Impinger Temp. (°F)	Vacuum on Sample Train ("Hg)
					Calc.	Actual		In	Out			
NEG	8						109					
	9 38						109					
	10 48						109					
	12 42	7:36	210.340				109					
	14 44	7:30	207.530	0.44	1.25	1.25	109	81	83	73	10.0	
	16 44	7:24	203.800	0.35	0.97	0.97	109	81	83	73	7.0	
	18 44	7:18	199.820	0.43	1.20	1.20	109	81	82	73	8.0	
	20 48	7:12	196.090	0.40	1.10	1.10	109	81	82	73	8.0	

[illegible]

SOURCE SAMPLING FIELD DATA SHEET

Plant CF CHEMICALSSampling Location D.A.P. INLET TO COOLER SCRUBBERDate 12/16/71 Run No. 1Time Start 5:30 Time End 6:21Sampling Time/Point 22 ft 5 inDB 140 °F, WB 100 °F, VF @ DP 92 "HgMoisture .05 %, FDA .95, Gas Density Factor .99Barometric Press 30 "Hg, Stack Press 29.71 "HgWeather Clear - WarmTemp. 80 °F, W/D —, W/S —Sample Box No. 1 Meter Box No. 1Meter ΔH 1.74 Pitot Corr. Factor 0.88Nozzle Dia. 1/4 in., Probe Length 6 ftProbe Heater Setting —Stack Dimensions: Inside Diameter 60 inInside Area 19.625 ft²Height 30 ft*

* = approx. above floor level

Sketch of Stack

121 min



Mat'l Processing Rate

Final Gas Meter Reading 715.590 ft³Initial Gas Meter Reading 635.011 ft³Total Condensate in Impingers 20 mlMoisture in Silica Gel 220.3 -197.5 = 22.8 gSilica Gel Container No. 209 Filter No. 72012Orsat: CO₂ 0O₂ 19.8CO —N₂ —Excess Air —Test Conducted By: R. DuranL. WurtsRemarks: *Fluorides*

Port and Traverse Point No.	Distance from End of Port (in)	Clock Time	Gas Meter Reading (ft ³)	Stack Velocity Head ("H ₂ O)	Meter Orifice Press. Diff. ("H ₂ O)		Stack Gas Temp. (°F)	Gas Sample Temp. @ Dry Gas Meter (°F)		Sample Box Temp. (°F)	Last Impinger Temp. (°F)	Vacuum on Sample Train ("Hg)
					Calc.	Actual		In	Out			
Port #1	5/8	4:20	635.011	—	—	—	—	—	—	—	—	—
2	2 1/8	4:25 1/2	639.7	1.10	4.05	2.35	140	112	112	—	104	22.5
3	3 1/4	4:31	644.4	0.65	2.40	2.30	—	112	112	—	—	22.5
4	4 1/4	4:36 1/2	648.4	0.40	1.50	1.50	—	113	112	—	—	8.5
5	6 1/4	4:42	652.1	0.35	1.35	1.35	—	113	112	—	—	7.0
6	8	4:47 1/2	655.8	0.35	1.35	1.35	—	113	112	—	—	7.0
7	9 5/8	4:53	659.5	0.33	1.25	1.25	—	113	112	—	—	6.5
8	11 5/8	4:58 1/2	663.0	0.33	1.25	1.25	—	113	112	—	—	6.5
9	13 7/8	5:04	666.7	0.33	1.25	1.25	—	113	112	—	—	7.0

Red #1

[illegible]

SOURCE SAMPLING FIELD DATA SHEET

Plant CF CHEMICALSSampling Location D.A.P. INLET GENERATOR COOLER SCRUBBERDate 12-18-71 Run No. 2Time Start 1:50 Time End 3:51Sampling Time/Point 22 pts. @ 5 1/2 min =DB 140 °F, WB — °F, VF @ DP — "HgMoisture .03 %, FDA .97, Gas Density Factor 0.98Barometric Press 30 "Hg, Stack Press 29.7 "HgWeather ClearTemp. 80 °F, W/D —, W/S —Sample Box No. 1 Meter Box No. 1Meter All 1.74 Pitot Corr. Factor 0.83Nozzle Dia. 1/4 in., Probe Length 6 ftProbe Heater Setting —Stack Dimensions: Inside Diameter 60 in
Inside Area 19.625 ft²
Height 30 ft*

* = approx. above floor level

Sketch of Stack

(N)

Mat'l Processing Rate —Final Gas Meter Reading 799.904 ft³Initial Gas Meter Reading 725.337 ft³Total Condensate in Impingers 12 mlMoisture in Silica Gel 206.1 - 185.6 gmSilica Gel Container No. 204 Filter No. 7202

Orsat:	CO ₂	<u>0</u>			
	O ₂	<u>20.3</u>			
	CO	<u>—</u>			
	N ₂				

Excess Air —Test Conducted By: R. DorganL. WurtsRemarks: "FLUORIDES"

Port and Traverse Point No.	Distance from End of Port (in)	Clock Time	Gas Meter Reading (ft ³)	Stack Velocity Head ("H ₂ O)	Meter Orifice Press. Diff. ("H ₂ O)		Stack Gas Temp. (°F)	Gas Sample Temp. @ Dry Gas Meter (°F)		Sample Box Temp. (°F)	Last Impinger Temp. (°F)	Vacuum on Sample Train ("Hg)
					Calc.	Actual		In	Out			
Port #1		1:50	725.337									
1	5/8	—	—	—	—	—	—	—	—	—	—	—
2	2 1/8	1:53 1/2	—	0.55	2.10	2.10	140	71	71	—	70	20.5
3	3 1/4	2:01	732.2	0.45	1.75	1.75		72	72	—		10.0
4	4 1/4	2:06 1/2	735.5	0.28	1.05	1.05		73	72	—		5.5
5	6 1/4	2:12	738.9	0.33	1.25	1.25		74	72	—		7.0
6	8	2:17 1/2	742.4	0.30	1.15	1.15		74	72	—		6.5
7	9 5/8	2:23	745.8	0.30	1.15	1.15		75	73	—		6.5
8	11 5/8	2:28 1/2	749.2	0.33	1.25	1.25		76	73	—		6.8
9	13 3/8	2:34	752.8	0.33	1.25	1.25		77	73	—		6.8

[illegible]

SOURCE SAMPLING FIELD DATA SHEET

Plant CF CHEMICALS - BARTON, FL

Sampling Location _____

Date 12-20-71 Run No. 3Time Start 6:00 Time End 8:01

Sampling Time/Point _____

DB 140 °F, WB — °F, VF @ DP — "HgMoisture .03%, FDA .97, Gas Density Factor 0.98Barometric Press 30 "Hg, Stack Press 24.71 "HgWeather Clear - WarmTemp. 80 °F, W/D —, W/S —Sample Box No. 1 Meter Box No. 1Meter Alls 1.74 Pitot Corr. Factor 0.83Nozzle Dia. 1/4 in., Probe Length 6 ftProbe Heater Setting —Stack Dimensions: Inside Diameter 60 in
Inside Area 19.625 ft²
Height 36 ft*

* = approx. above floor level

Sketch of Stack



Mat'l Processing Rate _____

Final Gas Meter Reading 902.421 ft³Initial Gas Meter Reading 815.805 ft³Total Condensate in Impingers 22 ml 748Moisture in Silica Gel 200.8-177 gm 3Silica Gel Container No. 1101 Filter No. 72030Orsat: CO₂ 0O₂ 20.0CO —N₂ _____

Excess Air _____

Test Conducted By: R. DurganL. Wurts

Remarks: _____

"Fluorides"

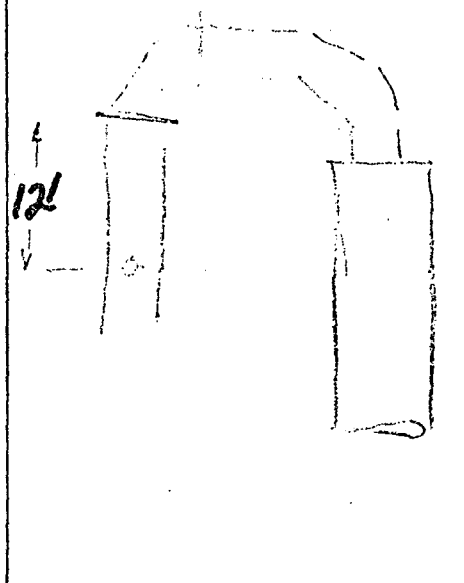
Port and Traverse Point No.	Distance from End of Port (in)	Clock Time	Gas Meter Reading (ft ³)	Stack Velocity Head ("H ₂ O)	Meter Orifice Press. Diff. ("H ₂ O)		Stack Gas Temp. (°F)	Gas Sample Temp. & Dry Gas Meter (°F)		Sample Box Temp. (°F)	Last Impinger Temp. (°F)	Vacuum on Sample Train ("Hg)
					Calc.	Actual		In	Out			
port #1		6:00	815.805									
1	58	—	—	—	—	—	—	—	—	—	—	—
2	2 1/8	6:05 1/2	818.9	1.05	3.90	1.50	140	87	88	—	75	22.5
3	3 1/4	6:11	823.1	0.65	2.45	2.20		86	87	—		20.5
4	4 3/4	6:16 1/2	827.6	0.57	2.15	2.15		86	87	—		20.5
5	6 1/4	6:22	832.0	0.48	1.85	1.85		86	86	—		10.0
6	8	6:27 1/2	—	0.45	1.75	1.75		86	86	—		10.0
7	9 5/8	6:33	840.0	0.48	1.85	1.85		86	86	—		10.0
8	11 5/8	6:38 1/2	844.2	0.48	1.85	1.85		86	85	—		12.0
9	13 7/8	6:44	848.4	0.48	1.85	1.85		86	85	—		11.5

[illegible]

SOURCE SAMPLING FIELD DATA SHEET

Plant CF CHEMICALS
 Sampling Location "P"
 Date 12-16-71 Run No. 1
 Time Start 4:32 Time End 6:29
 Sampling Time/Point 6.5 min @ 18 ft = 11.7
 DB — °F, WB — °F, VF @ DP — "Hg
 Moisture 10.5%, FDA 89.5 Gas Density Factor
 Barometric Press 30 "Hg, Stack Press 28.7 "Hg
 Weather Clear
 Temp. 80's °F, W/D _____, W/S _____
 Sample Box No. _____ Meter Box No. _____
 Meter ΔHe 1.72 Pitot Corr. Factor 0.83
 Nozzle Dia. 1/4 in., Probe Length 6 ft
 Probe Heater Setting 40%
 Stack Dimensions: Inside Diameter 60 in
 Inside Area _____ ft²
 Height _____ ft

Sketch of Stack



Mat'l Processing Rate _____

Final Gas Meter Reading 482.140 ft³Initial Gas Meter Reading 391.750 ft³Total Condensate in Impingers 200 mlMoisture in Silica Gel 221.0 - 193.5 = 27.5 gmSilica Gel Container No. 202 Filter No. 72014

Orsat: CO₂ _____
 O₂ 19.5 _____
 CO _____
 N₂ _____
 Excess Air _____

Test Conducted By: Ray Black
Addy Taylor

Remarks: _____

Port and Traverse Point No.	Distance from End of Port (in)	Clock Time	Gas Meter Reading (ft ³)	Stack Velocity Head ("H ₂ O)	Meter Orifice Press. Diff. ("H ₂ O)		Stack Gas Temp. (°F)	Gas Sample Temp. @ Dry Gas Meter (°F)		Sample Box Temp. (°F)	Last Impinger Temp. (°F)	Vacuum on Sample Train ("Hg)
					Calc.	Actual		In	Out			
#2	3/4		391.750									
1	2 3/8		—	0.25		0.8	126	88	88		81	2.5
2	4		—	0.34		1.1		92	89		84	2.5
3	5 7/8		—	0.22		2.7		94	90		84	2.5
4	7 3/4		399.9	0.85		2.8		-102	95		86	2.5
5	9 7/8		303.5	0.85		2.8		104	98		86	8.0
6	12 1/4		409.9	0.88		2.8		-106	100		88	8.0
7	15		415.5	0.65		2.1		112	104		90	6.0
8	18 3/8		421.7	0.77		2.5		116	108		88	6.0

[illegible]

SOURCE SAMPLING FIELD DATA SHEET

Plant C.F. Chemical
 Sampling Location 'P'
 Date Dec. 13, 1971 Run No. 2
 Time Start 1:46 Time End 3:43
 Sampling Time/Point 1.5 mi. S. 12.1 = 117
 DB °F, WB 114 °F, VF @ DP °F
 Moisture 11.5%, FID 88.5 Gas Density Factor
 Barometric Press 30 "Hg, Stack Press 28.7 "Hg
 Weather Clear
 Temp. °F, W/D , W/S
 Sample Box No. Meter Box No.
 Meter ΔH@ 1.72 Pitot Corr. Factor
 Nozzle Dia. 1/4 in., Probe Length 6 ft
 Probe Heater Setting 40%
 Stack Dimensions: Inside Diameter 60 in
 Inside Area ft²
 Height ft

Sketch of Stack

*See Run 1
for sketch*

Mat'l Processing Rate

Final Gas Meter Reading 597.956 ft³
 Initial Gas Meter Reading 492.610 ft³
 Total Condensate in Impingers 198 net 21.5
 Moisture in Silica Gel 219.5-196 gm (23.5)
 Silica Gel Container No. 216 Filter No. 72017
 Orsat: CO₂ 0
 O₂ 20.6
 CO 0
 N₂
 Excess Air

Test Conducted By: Ray Black
Eric Johnson

Remarks:

Port and Traverse Point No.	Distance from End of Port (in)	Clock Time	Gas Meter Reading (ft ³)	Stack Velocity Head ("H ₂ O)	Meter Orifice Press. Diff. ("H ₂ O)		Stack Gas Temp. (°F)	Gas Sample Temp. @ Dry Gas Meter (°F)		Sample Box Temp. (°F)	Last Impinger Temp. (°F)	Vacuum on Sample Train ("Hg)
					Calc.	Actual		In	Out			
1	34	—	492.610	—	—	—	—	—	—	—	—	—
2	238	6.5	496.1	0.31		1.10	100	68	68	—	59	5
3	4	13.0	500.5	0.45		1.50		80	70	—	58	6
4	578	19.5	505.6	0.65		2.15		80	71	—	59	8
5	734	26.0	510.8	0.65		2.15		95	73	—	59	8
6	978	32.5	516.3	0.75		2.45		104	78	—	60	9
7	1244	39.0	521.4	0.80		2.65		110	80	—	62	10
8	15	45.5	527.4	0.80		2.65		113	84	—	63	10
9	1878	52.0	532.0	0.95		3.15		120	89	—	64	11

[illegible]

SOURCE SAMPLING FIELD DATA SHEET

Plant CF Chemicals
 Sampling Location upr
 Date Dec. 20, 1971 Run No. 3
 Time Start 6:00 Time End 7:57
 Sampling Time/Point _____
 DB _____ °F, WB _____ °F, VF @ DP _____ "Hg
 Moisture 115 %, FD 88.5 Gas Density Factor _____
 Barometric Press 30 "Hg, Stack Press 287 "Hg
 Weather Clear
 Temp. 80's °F, W/D _____, W/S _____
 Sample Box No. _____ Meter Box No. _____
 Meter ΔH 1.72 Pitot Corr. Factor 0.33
 Nozzle Dia. 1/4 in., Probe Length 6 ft
 Probe Heater Setting _____
 Stack Dimensions: Inside Diameter 60 in
 Inside Area _____ ft²
 Height _____ ft

Sketch of Stack

See Run 1
for sketch

Mat'l Processing Rate _____

Final Gas Meter Reading 728.650 ft³Initial Gas Meter Reading 605.510 ft³Total Condensate in Impingers 162 mlMoisture in Silica Gel 205.5 - 1715 = 34 gm {96Silica Gel Container No. 213 Filter No. 72034

Orsat:	CO ₂	<u>0</u>			
	O ₂	<u>20.3</u>			
	CO	<u>0</u>			
	N ₂	<u>79.7</u>			

Excess
Air
 Test Conducted By: Ray Black
Tony Arroyo

Remarks: _____

Port and Traverse Point No.	Distance from End of Port (in)	Clock Time	Gas Meter Reading (ft ³)	Stack Velocity Head ("H ₂ O)	Meter Orifice Press. Diff. ("H ₂ O)		Stack Gas Temp. (°F)	Gas Sample Temp. @ Dry Gas Meter (°F)		Sample Box Temp. (°F)	Last Impinger Temp. (°F)	Vacuum on Sample Train ("Hg)
					Calc.	Actual		In	Out			
1	3/4	6:00	605.510	—	—	—	—	—	—	—	—	—
2	2 3/8	6:06 1/2	608.5	0.15	—	0.50	98	80	80	—	68	3.0
3	4	6:13	613.8	0.75	—	2.50	98	85	82	—	72	9.0
4	5 1/8	6:19 1/2	620.3	0.95	—	3.15	98	103	83	—	78	12.5
5	7 3/4	6:26	627.0	0.95	—	3.15	98	114	86	—	82	12.5
6	9 1/8	6:32 1/2	633.8	1.00	—	3.30	96	120	90	—	82	13.0
7	12 1/4	6:39	641.0	1.00	—	3.30	96	126	84	—	82	13.0
8	15	6:45 1/2	648.5	1.20	—	3.90	94	130	97	—	82	11.0
9	18 3/8	6:52	656.5	1.30	—	4.30	94	134	102	—	80	12.0

[illegible]

SOURCE SAMPLING FIELD DATA SHEET

Plant CF. CHEMICALS

Sampling Location DAP #3 (Between vector) SCURFER #112 (R) Sketch of Stack

Date 12-16-71 Run No. 2

Time Start _____ Time End _____

Sampling Time/Point 5 min/pt (Total = 110)

DB _____ °F, WB _____ °F, VF @ DP _____ "Hg

Moisture 6.4 %, FDA 0.97 Gas Density Factor _____

Barometric Press 30 "Hg, Stack Press 27 Hg

Weather Clear

Temp. _____ °F, W/D _____, W/S _____

Sample Box No. _____ Meter Box No. _____

Meter ΔH 1.70 Pitot Corr. Factor 0.83

Nozzle Dia 0.25 in., Probe Length 6 ft

Probe Heater Setting _____

Stack Dimensions: Inside Diameter 37.5 in

Inside Area 7.67 ft²

Height _____ ft

Mat'l Processing Rate _____

Final Gas Meter Reading 223.000 ft³

Initial Gas Meter Reading 096.800 ft³

1200 final - 200 initial = 1000 net

Total Condensate in Impingers 1000 ml

Moisture in Silica Gel 39 gm

Silica Gel Container No. 210 Filter No. 72-02

Orsat: CO₂ _____

O₂ 19.8

CO _____

N₂ _____

Excess Air _____

Test Conducted By: J. DOLLAR

A. WILSON

Remarks: _____

Port and Traverse Point No.	Distance from End of Port (in)	Clock Time	Gas Meter Reading (ft ³)	Stack Velocity Head ("H ₂ O)	Meter Orifice Press. Diff. ("H ₂ O)		Stack Gas Temp. (°F)	Gas Sample Temp. & Dry Gas Meter (°F)		Sample Box Temp. (°F)	Last Impinger Temp. (°F)	Vacuum o Samp Trail ("Hg)
					Calc.	Actual		In	Out			
		<u>1635</u>	<u>096.800</u>									
<u>1</u>	<u>14 1/2</u>	<u>1640</u>	<u>—</u>	<u>0.67</u>	<u>1.83</u>	<u>1.88</u>	<u>175</u>	<u>98</u>	<u>96</u>	<u>—</u>	<u>85</u>	
<u>2</u>	<u>2 1/8</u>	<u>1645</u>	<u>107.8</u>	<u>0.72</u>	<u>2.00</u>	<u>2.00</u>		<u>98</u>	<u>96</u>	<u>—</u>	<u>85</u>	
<u>3</u>	<u>2 1/8</u>	<u>1650</u>	<u>112.1</u>	<u>2.5</u>	<u>7.9</u>	<u>7.9</u>		<u>96</u>	<u>96</u>		<u>85</u>	
<u>4</u>	<u>3 1/8</u>	<u>1655</u>	<u>—</u>	<u>2.5</u>	<u>7.9</u>	<u>7.9</u>	<u>160</u>	<u>97</u>	<u>96</u>		<u>85</u>	
<u>5</u>	<u>4 1/8</u>	<u>1700</u>	<u>126.5</u>	<u>0.5</u>	<u>1.45</u>	<u>1.45</u>		<u>99</u>	<u>96</u>		<u>85</u>	<u>8.</u>
<u>6</u>	<u>6 1/8</u>	<u>1705</u>	<u>128.2</u>	<u>0.15</u>	<u>0.34</u>	<u>0.34</u>		<u>99</u>	<u>95</u>		<u>85</u>	<u>2.</u>
<u>7</u>	<u>7 1/4</u>	<u>1710</u>	<u>—</u>	<u>0.60</u>	<u>1.75</u>	<u>1.75</u>	<u>180</u>	<u>99</u>	<u>95</u>		<u>85</u>	<u>5.</u>
<u>8</u>	<u>8 3/8</u>	<u>1715</u>	<u>137.9</u>	<u>0.36</u>	<u>0.96</u>	<u>0.96</u>		<u>97</u>	<u>95</u>			<u>5.</u>



SOURCE SAMPLING FIELD DATA SHEET

Plant **C.F. CHEMICALS**Sampling Location **DAP #3** *Between Reactor #3 and Scrubber #1 + 2* Sketch of StackDate **12-18-71** Run No. **2**Time Start **1345** Time End **1538**Sampling Time/Point **5 min/pt (total=110)**

DB _____ °F, WB _____ °F, VF @ DP _____ "Hg

Moisture _____ %, FDA _____, Gas Density Factor _____

Barometric Press **30** "Hg, Stack Press **27** Hg

Weather _____

Temp. **72** °F, W/D _____, W/S _____

Sample Box No. _____ Meter Box No. _____

Meter ΔH_e _____ Pitot Corr. Factor _____

Nozzle Dia. _____ in., Probe Length _____ ft

Probe Heater Setting _____

Stack Dimensions: Inside Diameter **37.5** in
Inside Area _____ ft²
Height _____ ft

Mat'l Processing Rate _____

Final Gas Meter Reading **324.653** ft³Initial Gas Meter Reading **233.500** ft³

FINAL=1001 ml, INITIAL=700 ml, Net=301 ml

Total Condensate in Impingers **801** mlMoisture in Silica Gel **33.6** gmSilica Gel Container No. **221** Filter No. _____Orsat: CO₂ **0**O₂ **20.7**CO **0**N₂ _____

Excess Air _____

Air _____

Test Conducted By: **DOLLAR****SHOOTER****WILSON**Remarks: *Due to duct design suspect liquid entrainment especially in late series of points.*

Port and Traverse Point No.	Distance from End of Port (in)	Clock Time	Gas Meter Reading (ft ³)	Stack Velocity Head ("H ₂ O)	Meter Orifice Press. Diff. ("H ₂ O)		Stack Gas Temp. (°F)	Gas Sample Temp. & Dry Gas Meter (°F)		Sample Box Temp. (°F)	Last Impinger Temp. (°F)	Vacuum on Sample Train ("Hg)
					Calc.	Actual		In	Out			
		1345	233.500									
1		1350	236.9	1.0	1.85	1.85	170	71	71	-	78	
2		1355	243.8	1.0	1.85	1.85	170	72	72	-	74	
3		1400	244.5	0.9	1.70	1.70	170	72	72	-		
4		1405	248.2	0.9	1.70	1.70	170	70	73	-	80	
5		1410	252.0	0.45	0.85	0.85	170	70	73	-	80	
6		1415	253.7	0.15	0.22	0.22	170	71	72	-	80	
7		1420	255.2	0.05	-	-	170	71	72	-	80	
8		1425	256.6	0.15	0.22	0.22	170	71	72	-	80	

[illegible][illegible]

SOURCE SAMPLING FIELD DATA SHEET

at **C.F. CHEMICALS**Sampling Location Between Reactor Scrubbers

Sketch of Stack

Date 12-20-71 Run No. 3Time Start 1805 Time End 1959Sampling Time/Point 5 min (Total = 110)DB 169 °F, WB 105 °F, VF @ DP 10.8 "HgMoisture 0.35%, FDA 0.64 Gas Density FactorBarometric Press 30 "Hg, Stack Press 29 "HgWeather ClearTemp. 78 °F, W/D _____, W/S _____Sample Box No. 2 Meter Box No. _____Meter 4H3 1.70 Pitot Corr. Factor 0.83Nozzle Dia 0.25 in., Probe Length 6 ft

Probe Heater Setting _____

Stack Dimensions: Inside Diameter 37.5 inInside Area _____ ft²

Height _____ ft

Mat'l Processing Rate _____

Final Gas Meter Reading 410.800 ft³Initial Gas Meter Reading 324.700 ft³Total Condensate in Impingers 818 mlMoisture in Silica Gel 38 gmSilica Gel Container No. 219 Filter No. 72032Orsat: CO₂ 0.7O₂ 19.8

CO _____

N₂ _____

Excess _____

Air _____

Test Conducted By: J. DollarA. Wilson

Remarks: _____

Port and Traverse Point No.	Distance from End of Port (in)	Clock Time	Gas Meter Reading (ft ³)	Stack Velocity Head ("H ₂ O)	Meter Orifice Press. Diff. ("H ₂ O)		Stack Gas Temp. (°F)	Gas Sample Temp. @ Dry Gas Meter (°F)		Sample Box Temp. (°F)	Last Impinger Temp. (°F)	Vacuum on Sample Train ("Hg)
					Calc.	Actual		In	Out			
		1805										
1		1810	327.9	0.65	1.20	1.20	168	82	84	-	79	
2		1815	331.7	0.90	1.80	1.80	-	82	82	-	-	
3		1820	334.3	0.50	0.90	0.90	-	82	79	-	-	
4		1825	336.8	0.40	0.76	0.76	173	82	77	-	75	
5		1830	338.5	0.20	0.34	0.34	-	82	77	-	79	
6		1835	340.7	0.35	0.63	0.63	170	81	77	-	79	
7		1840	342.8	0.32	0.57	0.57	-	82	76	-	-	
8		1845	344.7	0.25	0.47	0.42	-	82	76	-	-	

SAME AS RUN NO. 2

AMMONIA EMISSIONS

SAMPLING DATA SHEET FOR Ammonia

Plant C.F. Chemicals, Inc. Stack DAP#3, Station "K"

Remarks Sampled by George Allen

Run No.	1	2	3
Date	12-16-71	12-18-71	12-20-71
Time of Sample	1855-1925	1605-1635	2015-2045
Barometric Pressure, "Hg	30	30	30
Stack Pressure, "Hg	29	29	29
Final Dry Test Meter Reading, Ft ³	011.711	014.824	017.751
Initial Dry Test Meter Reading, Ft ³	008.439	011.725	014.824
Meter Volume Sampled @ Meter Cond., Ft ³	3.272	3.099	2.927
Average Meter Temperature, °F	95	83	85
Average Stack Temperature, °F	164	170	170
Average Meter Vacuum, "Hg	—	—	—
Average Meter Orifice ΔH, "H ₂ O	—	—	—
Observed Sampling Rate, LPM	3.1	2.9	2.8
Gas Volume Sampled, Ft ³ , Dry, 70°F, 29.92 "Hg	3.132	3.032	2.853

Calculations:

SAMPLING DATA SHEET FOR Ammonia

Plant C.F. Chemicals, Inc. Stack DAP#3, Station "L"

Remarks Sampled by Tommy Tucker

Run No.	1	2	3
Date	12-16-71	12-18-71	12-20-71
Time of Sample	1900-1930	1630-1700	2000-2110
Barometric Pressure, "Hg	30	30	30
Stack Pressure, "Hg	29.7	29.7	29.7
Final Dry Test Meter Reading, Ft ³	158.440	258.098	353.565
Initial Dry Test Meter Reading, Ft ³	155.470	255.109	350.565
Meter Volume Sampled @ Meter Cond., Ft ³	2.970	2.989	3.000
Average Meter Temperature, °F	118	102	118
Average Stack Temperature, °F	160	150	151
Average Meter Vacuum, "Hg	—	—	—
Average Meter Orifice ΔH , "H ₂ O	0.07	0.06	0.06
Observed Sampling Rate, LPM	2.8	2.8	2.8
Gas Volume Sampled, Ft ³ , Dry, 70°F, 29.92 "Hg	2.730	2.826	2.758

Calculations:

SAMPLING DATA SHEET FOR Ammonia

Plant C.F. Chemicals, Inc. Stack DAP#3, Station "M"

Remarks Sampled by John Chadbourne

Run No.	1	2	3
Date	12-16-71	12-18-71	12-20-71
Time of Sample	1900-1930	1600-1630	2000-2030
Barometric Pressure, "Hg	30	30	30
Stack Pressure, "Hg	28.1	28.1	28.1
Final Dry Test Meter Reading, Ft ³	96.437	100.530	103.580
Initial Dry Test Meter Reading, Ft ³	93.253	97.400	100.566
Meter Volume Sampled @ Meter Cond., Ft ³	3.184	3.130	3.014
Average Meter Temperature, °F	95	76	83
Average Stack Temperature, °F	132	111	111
Average Meter Vacuum, "Hg	—	—	—
Average Meter Orifice ΔH , "H ₂ O	—	—	—
Observed Sampling Rate, LPM	3.0	3.0	2.8
Gas Volume Sampled, Ft ³ , Dry, 70°F, 29.92 "Hg	3.048	3.103	2.949

Calculations:

SAMPLING DATA SHEET FOR Ammonia

Plant C.F. Chemicals, Inc. Stack DAP# 3, Station "N"

Remarks Sampled by Bob Durgan

Run No.	1	2	3
Date	12-16-71	12-18-71	12-20-71
Time of Sample	1900-1930	1603-1633	2005-2055
Barometric Pressure, "Hg	30	30	30
Stack Pressure, "Hg	29.7	29.7	29.7
Final Dry Test Meter Reading, Ft ³	003.520	007.159	10.291
Initial Dry Test Meter Reading, Ft ³	000.610	003.543	7.170
Meter Volume Sampled @ Meter Cond., Ft ³	2.910	3.616	3.121
Average Meter Temperature, °F	90	86	88
Average Stack Temperature, °F	140	140	140
Average Meter Vacuum, "Hg	—	—	—
Average Meter Orifice ΔH, "H ₂ O	—	—	—
Observed Sampling Rate, LPM	2.7	3.4	2.9
Gas Volume Sampled, Ft ³ , Dry, 70°F, 29.92 "Hg	2.811	3.519	3.026

Calculations:

SAMPLING DATA SHEET FOR Ammonia

Plant C.F. Chemicals, Inc. Stack DAP #3, Station "P"

Remarks Sampled by Ray Black

Run No.	1	2	3
Date	12-16-71	12-18-71	12-20-71
Time of Sample	1945-2015	1615-1645	2020-2050
Barometric Pressure, "Hg	30	30	30
Stack Pressure, "Hg	28.7	28.7	28.7
Final Dry Test Meter Reading, Ft ³	486.878	605.365	732.716
Initial Dry Test Meter Reading, Ft ³	483.540	601.318	728.814
Meter Volume Sampled @ Meter Cond., Ft ³	3.338	4.047	3.902
Average Meter Temperature, °F	98	110	123
Average Stack Temperature, °F	124	100	95
Average Meter Vacuum, "Hg	—	—	—
Average Meter Orifice ΔH, "H ₂ O	0.06	0.06	0.06
Observed Sampling Rate, LPM	3.2	3.8	3.7
Gas Volume Sampled, Ft ³ , Dry, 70°F, 29.92 "Hg	3.178	3.772	3.556

Calculations:

SAMPLING DATA SHEET FOR Ammonia

Plant C.F. Chemicals, Inc. Stack DAP#3, Station "R"

Remarks Sampled by John Dollar

Run No.	1	2	3
Date	12-16-71	12-18-71	12-20-71
Time of Sample	1856-1927	1551-1621	1912-1923
Barometric Pressure, "Hg	30	30	30
Stack Pressure, "Hg	29	29	29
Final Dry Test Meter Reading, Ft ³	010.400	014.050	016.900
Initial Dry Test Meter Reading, Ft ³	007.400	010.500	014.100
Meter Volume Sampled @ Meter Cond., Ft ³	3.000	3.550	2.800
Average Meter Temperature, °F	98	88	98
Average Stack Temperature, °F	174	171	173
Average Meter Vacuum, "Hg	—	—	—
Average Meter Orifice ΔH, "H ₂ O	—	—	—
Observed Sampling Rate, LPM	2.7	3.3	2.6
Gas Volume Sampled, Ft ³ , Dry, 70°F, 29.92 "Hg	2.856	3.442	2.666

Calculations:

APPENDIX C

Standard Analytical Procedures

ENVIRONMENTAL PROTECTION AGENCY

Research Triangle Park, North Carolina 27711

Reply to
Attn of:

Date: 12-21-72

Subject: Summary of Fluoride Analysis

To: R. Neulicht, EMB, IRL

This memorandum is in response to your request for a brief summary of our SPADNS-Zirconium Lake procedure for determination of fluoride in stack emission samples.

Samples received in our laboratory are filtered through fluoride free paper filters to yield water soluble and water insoluble portions. The water insoluble particulate collected on the filter is rinsed thoroughly to be sure that all water soluble fluoride is rinsed through. The water soluble fraction is distilled from sulfuric acid to a maximum temperature of 180°C. If chloride is suspected in the sample Ag_2SO_4 is added to the still. SPADNS solution is added to an aliquot of the distillate and the absorbance is read at 570 nm. The concentration of the sample is determined from a calibration curve prepared from standard fluoride solutions. It is very important that the temperature of the samples be the same as that of the standards when absorbances are recorded.

The water insoluble fraction of the sample is evaporated to dryness in the presence of a slurry of CAO, and then fused with NaOH. The fusate is dissolved with distilled water, neutralized with dilute H_2SO_4 , distilled and analyzed as described for the soluble portion.

Paper filters containing particulate are cut into small pieces, suspended in a slurry of CAO, evaporated to dryness and ashed prior to the alkali fusion and distillation.

If you have any questions about this procedure, let me know.

Howard L. Crist

Howard L. Crist
Chief, Source Sample Analysis Section
SSFAB, QAEML

cc: R. E. Lee

Ammonia Determination Summary by
Modified Kjeldahl Distillation

An aliquot of sample containing no more than 10 mg ammonia is added to a Kjeldahl distillation assembly that has been cleaned out by distillation of ammonia-free distilled water for thirty minutes. Additional water is added, if necessary, to bring the volume in the flask to 150 ml. Phenolphthalein indicator is added and a solution of sodium hydroxide-sodium thiosulfate is added dropwise until the sample is basic to phenolphthalein. A phosphate buffer is then added to maintain a pH of 7.4.

The sample is heated until 100 ml of distillate is collected in 2 percent boric acid containing an indicator.

The distillation is continued using fresh 2 percent boric solution and distillate is collected until there is no color change of the boric acid.

The boric acid containing the ammonia is then titrated with standard sulfuric acid.

Phosphorous Pentoxide Determination

Colorimetric Molybdovanadophosphate Method

An aliquot of sample is hydrolyzed in the presence of HCl and HNO_3 acids by boiling almost to dryness.

The sample is cooled to room temperature, transferred to a 250 ml volumetric flask and diluted to volume with distilled water. A 20 ml aliquot is transferred to a 100 ml volumetric flask, 20 ml of molybdovanadate reagent is added and the flask is diluted to volume.

The absorbance of the yellow color is determined after ten minutes at 400 nm. The concentration of phosphorous pentoxide is determined from a calibration curve prepared with standard solutions.

APPENDIX D

Laboratory Results

ENVIRONMENTAL PROTECTION AGENCY
Research Triangle Park, North Carolina 27711

Reply to
Attn of:

Date: 2/4/72

Subject: Fluoride Analysis Central Farmers Chemical Inc.

To: .Mr. Jerome J. Rom
Emission Testing Branch
Division of Applied Technology
THROUGH: Mr. Howard Crist
SSAS, SSFAB, DAS

Attached is the Fluoride Data for the Central Farmer Chemical Inc. The water soluble fluoride was done by sulfuric acid distillation followed by the SPADNS-ZIRCONIUM Lake Method.

The products were fussed with NaOH followed by sulfuric acid distillation then by the SPADNS-ZIRCONIUM Lake Method.

Allen E. Riley
Allen E. Riley
Source Sample Analysis
Section, SSFAB, DAS

Attachment

cc: R. Lampe
J. McGinnity
J. Reynolds
D. von Lehmden
R. E. Lee, Jr.

FLUORIDE DATA

		Central Farmer Chemical		
		STATION	PH	
239	PF	Gaseous F ⁻	K	7.0 mg/Sample
240	PF	Gaseous F ⁻	L	5.8 mg/Sample
241	"	" "	M	8.8 mg/Sample
242	"	" "	N	0.77 Mg/Sample
243	"	" "	P	0.20 mg/Sample
244	"	" "	R	0.38 mg/Sample
245	"	Total Sample	R	143 mg/Sample
328	"	Filter		
248	"	Total Sample	K	67 mg/Sample
329	"	Filter		
249	"	Total Sample	L	154 mg/Sample
330	"	Filter		
250	"	Total Sample	M	2.4 mg/Sample
331	"	Filter		
251	"	Total Sample	N	34 mg/Sample
332	"	Filter		
252	"	Total Sample	P	2.8 mg/Sample
333	"	Filter		
253	"	Reactor Scrubber # 2		
		H ₂ O Inlet		2.5
254	"	" " #1		20.3 g/L
		" " "		3.3
255	"	30% Phos. Acid		19.7 g/L
263	"	54% Phos. Acid		28.4 g/L
256	"	DAP Product		13.6 g/L
298	"	H ₂ O Blank		22.7 mg/g
270	"	Probe Wash		19 µg/120 ml
271	"	Impinger	R	71 mg/Sample
272	"	Filter		
273	"	Total Sample	K	147 mg/Sample
339	"	Filter		
274	"	Total Sample	L	91. mg/Sample
338	"	Filter		

Moisture Run

Run #1

Run

Run #2

Run

FLUORIDE DATA
Central Farmer Chemical

			<u>STATION</u>	<u>PH</u>	
275	PF	Total Sample	M		8.1 mg/ Sample
342	"	Filter			
276	"	Total Sample	N		25 mg/ Sample
337	"	Filter			
277	"	Total Sample	P		4.6 mg/Sample
341	"	Filter l			
278	"	Reactor Scrubber #2			
		H ₂ O Inlet		2.8	20.7 g/L
279	"	" " # 1			
		H ₂ O Inlet		3.3	21.6 g/L
280	"	gone 30 % Phos. Acid			
281	"	54 % " "			15.5 g/L
282	"	DAP-Product			22.0 mg/g
299	"	H ₂ O Blank			25. µg/187 ml
300	"	Total Sample	R		319 mg/Sample
346	"	Filter			
301	"	Total Sample	K		57 mg/Sample
345	"	Filter			
302	"	Total Sample	L		22.6 mg/Sample
347	"	Filter			
303	"	Total Sample	M		1.2 mg/Sample
348	"	Filter			
336	"	Probe Wash	N		31 mg/Sample
304	"	1st. Impinger			
305	"	2nd. Impinger			
306	"	3rd. Impinger			
307	"	Filter	P		2.7 mg/sample
308	"	Total Sample			
349	"	Filter			
309	"	Reactor Scrubber #2			
		H ₂ O Inlet		3.4	15.6 g/L
310	"	" " #1			
		H ₂ O Inlet		5.2	9.6 g/L

FLUORIDE DATA
Central Farmer Chemical

311	gone	30% Phos. Acid	
312		54 % " "	14.7 g/L
313		DAP-Product	22.0 mg/g
326		H ₂ O Blank	18 µg/240 ml

ENVIRONMENTAL PROTECTION AGENCY

Research Triangle Park, North Carolina 27711

Reply to
Attn of:

Date: 2/15/72

Subject: Fluoride Analysis, Central Farmer Chemical Inc.

To: Mr. Jerome J. Rom
Emission Testing Branch
Division of Applied Technology
THROUGH: Mr. Howard Crist
SSAS, SSFAB, DAS

Attached is the fluoride data for Central Farmer Chemical Inc. The water insoluble were first fused with NaOH followed by sulfuric acid distillation then by the SPADNS-ZIRCONIUM Lake Method.

Allen E. Riley

Allen E. Riley
Source Sample Analysis
Section, SSFAB, DAS

Attachment

cc: R. Lampe
J. McGinnity ✓
J. Reynolds
D. von Lehmden
R. Lee, Jr.
H. Crist

CENTRAL FARMER CHEMICAL INC.

Insoluble Fluoride

<u>Sample Number</u>			<u>Sample</u>
250, 331	PF	66	µg/Sample
251, 332	PF	30.2	mg/Sample
252, 333	PF	0	
270, 271, 272	PF	20.3	mg/Sample
273, 339	PF	0.77	mg/Sample
274, 338	PF	50	mg/Sample
275, 342	PF	0.42	mg/Sample
276, 337	PF	18.5	mg/Sample
277, 341	PF	71	µg/Sample
300, 346	PF	54	mg/Sample
302, 347	PF	15.3	mg/Sample
303, 348	PF	0.21	mg/Sample
336, 304, 305	PF	17.6	mg/Sample
306, 307	PF	51	µg/Sample
308, 349	PF	21.4	mg/Sample
245, 328	PF	0.67	mg/Sample
248, 329	PF	62	mg/Sample
249, 330	PF	7.3	mg/Sample
301, 345	PF		

ENVIRONMENTAL PROTECTION AGENCY
Research Triangle Park, North Carolina 27711

Reply to
Attn of:

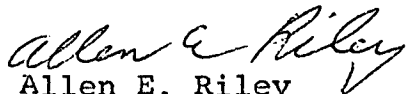
Date: 4/4/72

Subject: Determination of Ammonia in Stack Gas

To: Mr. Jerome J. Rom
Emission Testing Branch
Division of Applied Technology

Thru: Mr. Howard Crist, Chief,
Source Sample Analysis Section

Attached is the Ammonia Data for Central Farmer
Chemical Inc. The modified Kjeldahl distillation method
was used.


Allen E. Riley
Source Sample Analysis Section
SSFAB, DAS

cc: R. Lampe
J. McGinnity
J. Reynolds
D. von Lehmden
H. Crist

AMMONIA DATA FOR CENTRAL FARMER CHEMICAL INC.*

Run	Sample Number	Station	EPA Sample ML	EPA Mg/Sample	Total Sample ML	Total mg/Sample
1	257 PF	R	110	46.8	136	57.9
	258 "	K	80	1.0	107	1.3
	259 "	L	110	135.9	138	170.5
	260 "	M	110	<0.03	135	<.04
	261 "	N	68	16.8	94	23.2
	262 "	P	91	1.2	118	1.6
2	283 "	R	118	1010.9	148	1267.9
	284 "	K	64	1.2	95	1.8
	285 "	L	108	99.9	137	126.7
	286 "	M	81	1.3	122	2.0
	287 "	N	47	<0.03	77	<.05
	288 "	P	203	0.9	231	1.0
3	314 "	R	210	230.0	235	257.4
	315 "	K	79	0.2	105	0.3
	316 "	L	99	128.0	124	160.3
	317 "	M	70	0.7	97	1.0
	318 "	N	72	0.1	98	0.1
	319 "	P	123	0.2	149	0.2

*Samples were split with company

ENVIRONMENTAL PROTECTION AGENCY
Research Triangle Park, North Carolina 27711

✓
File

Reply to
Attn of:

Date: 2/29/72

Subject: Density at 76°F

To: Mr. Jerome J. Rom
Emission Testing Branch
THROUGH: Mr. Howard Crist
SSAS, SSFAB, DAS

Attached is the Density of the scrubber water samples
from Central Farmer Chemical Inc., which completes the
analysis of all samples.

Allen E. Riley
Allen E. Riley
Source Sample Analysis
Section, SSFAB, DAS

Attachment

cc: Mr. R. Lampe
Mr. J. McGinnity ✓
Mr. J. Reynolds
Mr. D. von Lehmden
Mr. H. Crist

FLUORIDE DATA
Central Farmer Chemical

<u>Number</u>	<u>Description</u>	<u>Density at 76°F</u>
156 PF	Scrubber H ₂ O Inlet	1.030
157 PF	Scrubber H ₂ O Outlet	1.026
158 PF	Flask cooler H ₂ O	1.020
159 PF	Hotwell Evap. H ₂ O	1.024
178 PF	Scrubber H ₂ O Inlet	1.028
179 PF	Scrubber H ₂ O Outlet	1.031
180 PF	Flask Cooler H ₂ O	1.026
181 PF	Hotwell Evap. H ₂ O	1.031
200 PF	Scrubber H ₂ O Inlet	1.029
201 PF	Scrubber H ₂ O Outlet	1.021
202 PF	Flask Cooler H ₂ O	1.026
203 PF	Hotwell Evap. H ₂ O	1.028
253 PF	Reactor Scrubber # 2 H ₂ O Inlet	1.269
254 PF	Reactor Scrubber # 1 H ₂ O Inlet	1.212
278 PF	Reactor Scrubber # 2 H ₂ O Inlet	1.067
279 PF	Reactor Scrubber # 1 H ₂ O Inlet	1.188
309 PF	Reactor Scrubber # 2 H ₂ O Inlet	1.193
310 PF	Reactor Scrubber # 1 H ₂ O Inlet	1.202

(Must be filled out for each test run)

Sampling Date 7/1/21 Yr. 21 Mo. 1 Day 1

First Ident.

No. Used

172 PF

Last Ident.

No. Used

301 PF

Test No.

72-6136
72-6137

Run No.

RECD.

RCRD.

9-19/21

Industry

Phosphate Fertilizer
(Use Table A)

UNIT PROCESS/OPERATION

WPPA, DAP

Company

C. F. Chemicals

AIR POLLUTION CONTROL

Address

EPA

FUEL USED

INLET ☐

Sampling Method

OUTLET ☐

GAS VOLUME SAMPLED

(METER VOL. IN FT³)

P. O.

LAB.

FILED

COPIES TO

Ident. No.

Description of
Sample or Sample
Fraction

Sample
Wt. Vol.
(Solid) (Liquid)
mg ml

Analysis Requested - General Comments
(approx. concentrations-possible interferences
etc.) (Indicate specific analysis on backside)

172 PF

194 PF

218 PF

245 PF

248 PF

271 PF

273 PF

300 PF

301 PF

P2 O5

COMMENTS:

SAMPLING

CONTRACTOR

(if applicable)

PROJECT OFFICER

Roy M. H. R.

REQUEST

REVIEWED BY

DATE ANALYSIS REQUESTED

(Must be filled out for each test run)

Sampling Date 7/1/21 12 12

First Ident.

No. Used

172 PF

Last Ident.

No. Used

301 PFTest No. 72 C1 36
72 C1 37

Run No. _____

RECD. _____

ROND. 9-19/21

INDUSTRY

Phosphate Fertilizer
(Use Table A)

UNIT PROCESS/OPERATION

WPPA, DAP

COMPANY

C. F. Chemicals

AIR POLLUTION CONTROL

COPIES TO

ADDRESS

FUEL USED

P. O. _____

SAMPLING

METHOD

EPAINLET ☐OUTLET ☐GAS VOLUME SAMPLED
(METER VOL. IN FT³)

LAB. _____

FILED _____

Ident. No.	Description of Sample or Sample Fraction	Sample		Analysis Requested - General Comments (approx. concentrations-possible interferences etc.) (Indicate specific analysis on backside)
		Wt. (Solid) mg	Vol. (Liquid) ml	
<u>172 PF</u>				<u>P2 O5</u>
<u>194 PF</u>				"
<u>218 PF</u>				"
<u>245 PF</u>				"
<u>248 PF</u>				"
<u>271 PF</u>				"
<u>273 PF</u>				"
<u>300 PF</u>				"
<u>301 PF</u>				"
COMMENTS: _____				

SAMPLING
CONTRACTOR _____

(if applicable)

PROJECT OFFICER

Roy Neuhoff

REQUEST

REVIEWED BY _____

DATE ANALYSIS REQUESTED _____

Trace Elements
ppm - for solid samples
µg/ml - for liquid samples

Mark (X) in block to left of Ident. No. when
requesting all analysis on that line

[illegible]

Analysis Method: 1-RDA, 2-SMIS, 3-OES, 4-PA, 5-ASV, 6-XRF, and 7- other

Comments:

Other Analysis - Use Table B to fill analysis requested (above each column)

Mark (x) for specific analysis requests

[illegible]

Comments:

Sampling Date 71 12 17
Yr. Mo. Day

No. Used 328FF

No. Used 346 PF

Run No.

RCRD. 9/14/72

Phosphate Fertilizers
(Use Table A)

W FPA DAF

C. F. Chemical

COPIES TO

P. O.

ΕΡΑ

INLET ☐

GAS VOLUME SAMPLED-
(METER VOL. IN FT³)

TAB.

FILED

C. DATES:

SAMPLING
CONTRACTOR

(if applicable)

PROJECT OFFICER

REQUEST

REVIEWED BY

DATE ANALYSIS REQUESTED

First loent.

No. Used

328PF

Last Ident.

No. Used

346 PF

Test No. 72 CI 36

Run No.

RECD.

RCRD.

INDUSTRY

COMPANY

ADDRESS

SAMPLING

METHOD

UNIT PROCESS/OPERATION

AIR POLLUTION CONTROL

FUEL USED

INLET ☐

OUTLET []

GAS VOLUME SAMPLED-

(METER VOL. IN FT³)

COPIES TO

P. O.

TAB.

11:50

Ident. No.	Description of Sample or Sample Fraction	Sample Wt. (Solid) mg	Sample Vol. (Liquid) ml	Analysis Requested - General Comments (approx. concentrations-possible interferences etc.) (Indicate specific analysis on backside)
328PF				P2O5
329PF				..
339PF				..
346PF				..
345PF				..

COMMENTS:

SAMPLING

CONTRACTOR

(if applicable)

PROJECT OFFICER

REQUEST

REVIEWED BY

DATE ANALYSIS REQUESTED

µg/ml - for liquid samples

Mark (X) in block to left of Ident. No. when requesting all analysis on that line.

[illegible]

Comments:

Mark (x) for specific analysis req:

[illegible]

Comments:

APPENDIX E
PROJECT PARTICIPANTS

PROJECT PARTICIPANTS AND TITLES

Environmental Engineering, Inc.

<u>Name</u>	<u>Title</u>
Robert Sholtes	Project Director
John Dollar	Project Manager
Dennis Falgout	Project Engineer
John Chadbourne	Environmental Specialist
Tommy Tucker	Environmental Specialist
Ray Black	Environmental Specialist
Robert Durgan	Environmental Specialist
George Allen	Environmental Specialist
A.L. Wilson	Environmental Specialist
Bill Demery	Environmental Specialist
Mike Jackson	Environmental Specialist
Eric Johnson	Environmental Specialist
Larry Wurts	Environmental Specialist
Andy Taylor	Environmental Specialist
Jim Tscherfing	Chemist
Robert Maxwell	Chemist
Tony Arroyo	Computer Analyst

Environmental Protection Agency

Jerome Rom	EPA
John Reynolds	EPA
Roy Neulicht	EPA