

MRI REPORT

SOURCE TESTING REPORT
EMB Project No. 73-FRT-1

ARCO Chemical Company
Fort Madison, Iowa

Midwest Research Institute
Kansas City, Missouri 64110

EPA Contract 68-02-0228, Task 22

MRI Project No. 3585-C, Task No. 23

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by

E. P. Shea

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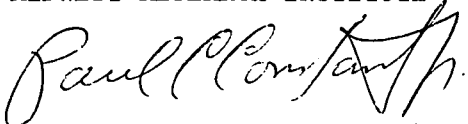
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PREFACE

The work reported herein was conducted by Midwest Research Institute (MRI) pursuant to a task order issued by the Environmental Protection Agency (EPA) under the terms of EPA Contract No. 68-02-0228. Mr. E. P. Shea served as the Project Chief and directed the MRI field team consisting of Messrs. Henry Moloney, Acid and Water Sampler; William Maxwell, Engineering Technician; Reid Flippin, Testing Engineer; Michael Bechtold, Engineering Technician; and William Cunningham, Laboratory Technician. Mr. Winton Kelly, EPA, was Project Officer and Mr. Lee Beck was the Field Engineer responsible for collecting process data. Mr. E. P. Shea prepared this final report.

Approved for:

MIDWEST RESEARCH INSTITUTE

A handwritten signature in cursive script, reading "Paul C. Constant, Jr.", written in dark ink.

Paul C. Constant, Jr.
Program Manager

TABLE OF CONTENTS

	<u>Page</u>
I. Introduction	1
II. Summary of Results	2
III. Process Description and Operation.	9
IV. Location of Sampling Ports	11
V. Sampling and Analytical Procedures	13
A. Fluorides.	13
B. Ammonia.	15
C. Integrated Gas Samples	15
Appendix A - Fluoride Results.	18
Appendix B - Gaseous Results	29
Appendix C - Operations Results.	36
Appendix D - Field Data.	38
Appendix E - Laboratory Report	75
Appendix F - Test Log.	104
Appendix G - Project Participants and Titles	106

LIST OF TABLES

<u>Table</u>	<u>Title</u>	<u>Page</u>
I	Summary of Results - Total Catch	4
II	Weight Results - Fluoride Runs	5
III	Analysis Results - Fluoride Runs	6
A-I	Fluoride Emission Data	19
A-II	Example Fluoride Calculations.	20
A-III	Fluoride Data and Calculated Values.	24
B-I	Summary of Results - Ammonia	30
B-II	Ammonia Emission Data.	31
B-III	Ammonia Data and Calculated Values	32
C-I	Production Rate.	37
F-I	Sampling Log	105

LIST OF FIGURES

<u>Figure</u>	<u>Title</u>	<u>Page</u>
1	DAP Plant Effluent Stack and Platform.	12
2	Location of Liquid Samples	14
3	Integrated Gas Sampling Train.	16

I. INTRODUCTION

Under the Clean Air Act as amended, the Environmental Protection Agency is charged with the establishment of performance standards for stationary source categories which may contribute significantly to air pollution. A performance standard is a standard for emissions of air pollutants which reflect emission limitations attainable through the best emission reduction systems that have been adequately demonstrated (taking into account economic considerations).

The development of realistic performance standards requires accurate data on pollution emissions within the various source categories. The objective of this project was to collect the data on emissions of fluoride and ammonia at a diammonium phosphate fertilizer plant. The ARCO Chemical Company plant at Fort Madison, Iowa, was designated by EPA as representative of a well controlled plant and was therefore selected for the emission testing program. This report presents the results of the tests run at the fertilizer plant to determine the fluoride and ammonia emissions.

On Monday, 19 March 1973, the equipment and personnel arrived at the site. The platform erection was not finished. On Tuesday, 20 March 1973, the equipment was unloaded at the stack and the laboratory. The support rails were installed on Ports 1 and 2, but not on Ports 3 and 4. The platform uprights used to fasten the support rails were not located properly and ARCO maintenance people had to be recalled to change the uprights. A preliminary velocity and temperature traverse was run Tuesday on Ports 1 and 2. The moisture determination run was not successful, so an assumed moisture value was used in setting

up the nomograph for Run No. 1 on Wednesday, 21 March 1973. The assumed value of 20% was about three times the actual moisture. This erroneous assumption resulted in Run No. 1 having an 88.6 isokinetic value. The other four runs using a 7% moisture value had isokinetic values of 98.3, 103.2, 100.9, and 105.3

On Tuesday, 20 March 1973, we were informed by the project officer that sampling for ammonia was to be conducted if possible. We had enough equipment to do this and we were able to get sulfuric acid from ARCO so we ran five tests for fluoride and four additional tests for ammonia. The results of these tests are included in this report. The samples were collected and packaged in polypropylene sample jars and given to the project officer for delivery to the EPA analytical laboratory.

On Friday, 23 March 1973, we ran three tests--one fluoride, one ammonia, and one integrated gas sample--removed the equipment from the stack, loaded the truck, and cleared the site. On Saturday, 24 March 1973, the crew returned to Kansas City.

II. SUMMARY OF RESULTS

Table I presents a summary of results from the fluoride runs. The fluoride caught in the cyclone ranged from 0.00 to 0.2 lb/hr with an average emission of 0.108 lb/hr. The fluoride per ton of P_2O_5 ranged from 0.0 to 0.0123 lb/ton with an average of 0.007 lb/ton. The fluoride detected was present in the soluble form in the cyclone catch from all five runs. The

analysis for insoluble fluoride showed less than 0.06 mg which is the lower limit of detection for the analytical method used.

Total fluorides caught during each of the five emission tests are in Table I. As was the case in the cyclone catch, only soluble fluoride was detected from all runs except No. 4. In Run No. 4 there was 0.08 mg of insoluble fluoride detected. The total fluoride emitted ranged from 0.39 lb/hr to 0.85 lb/hr with an average emission of 0.554 lb/hr of fluoride. Table I also shows the emissions per ton of P_2O_5 processed. It ranges from 0.0758 lb/ton to 0.0555 lb/ton with average of 0.0356 lb/ton.

Table I shows also the results of the moisture and Orsat analysis of the stack gases for each fluoride run. The moisture varied from 5.4% to 7.5% with an average of 6.5%. There was no detectable CO present. The CO_2 content of the stack gas varied from 0.2% to 0.6%, with an average of 0.34%. The average oxygen content for the five runs was 20.58%, with a variance from 20.2% to 21.0%.

Table II shows the weight of fluoride collected in each emission test. The data as presented show the soluble and insoluble fluoride caught in the cyclone and soluble and insoluble fluorides in the total catch.

The analytical results for the scrubber liquid samples, the feed and product samples, are presented in Table III.

For the four ammonia runs, the analytical results show that there was no detectable ammonia discharged from the DAP stack during the test period. All of the analyses show < 0.3 mg of ammonia. The lower detection limit for the analytical method is 0.3 mg of ammonia. Using the average

TABLE I

SUMMARY OF RESULTS - TOTAL CATCH

NAME	DESCRIPTION	UNITS	1F	2F	3F	4F	5F
	DATE OF RUN		03-21-73	03-21-73	03-22-73	03-22-73	03-23-73
QS	STK FLOWRATE, DRY, STD CN	DSCFM	135060	142550	129498	138549	116248
QA	ACTUAL STACK FLOWRATE	ACFM	156408	165428	151009	158642	135750
PMOS	PERCENT MOISTURE BY VOL		6.5	6.6	6.5	5.4	7.5
PCO2	PERCENT CO2 BY VOL, DRY		.3	.6	.2	.4	.2
P02	PERCENT O2 BY VOL, DRY		20.5	21.0	20.2	20.6	20.6
PCO	PERCENT CO BY VOL, DRY		0.0	0.0	0.0	0.0	0.0
	PROCESS FEED RATE	TONS P ₂ O ₅ /HR	14.0	15.3	18.2	16.2	14.6

FLUORIDES -- CYCLONE CATCH

MF	FLUORIDE WT-CYCLONE	MG	.50	.70	.10	.80	0.0
CAN	FLUORIDE LOAD-PTL, STD CN	GR/DSCF	.00012	.00015	.00002	.00017	--
CAT	FLUORIDE LOAD-PTL, STK CN	GR/ACF	.00011	.00013	.00002	.00015	--
CAW	FLUORIDE EMIS-CYCLONE	LB/HR	.14	.18	.02	.20	--
	FLUORIDE EMISSIONS	LB/TON P ₂ O ₅	0.01	0.0117	0.001	0.0123	0.0
MT	FLUORIDE WT-TOTAL	MG	1.70	3.30	1.90	2.28	1.60
CAO	FLUORIDE LOAD-TTL, STD CN	GR/DSCF	.00042	.00070	.00042	.00048	.00039
CAU	FLUORIDE LOAD-TTL, STK CN	GR/ACF	.00036	.00060	.00036	.00042	.00033
CAX	FLUORIDE EMIS-TOTAL	LB/HR	.49	.85	.47	.57	.39
	FLUORIDE EMISSIONS	LB/TON P ₂ O ₅	0.035	0.0555	0.0258	0.0351	0.0267
IC	PERC IMPINGER CATCH		71.4	78.8	95.7	64.9	100.0

TABLE II

WEIGHT RESULTS - FLUORIDE RUNS

<u>Run Number</u>	<u>Cyclone Catch Weight (mg)</u>			<u>Total Weight (mg)</u>		
	<u>Soluble Fluorides</u>	<u>Insoluble Fluorides</u>	<u>Total Fluorides</u>	<u>Soluble Fluorides</u>	<u>Insoluble Fluorides</u>	<u>Total Fluorides</u>
1F	0.5	--	0.5	1.7	--	1.7
2F	0.7	--	0.7	3.3	--	3.3
3F	0.1	--	0.1	1.9	--	1.9
4F	0.8	--	0.8	2.2	0.08	2.28
5F	--	--	--	1.6	--	1.6

TABLE III

ANALYSIS RESULTS - FLUORIDE RUNS

Run No.	Sample Identification No.	Description of Sample	Total Fluorides	P ₂ O ₅	pH	Ammonia
1F	503	Venturi scrubber inlet liquor (26% H ₃ PO ₄)	17.3 gm/l		0.52	
	504	Venturi scrubber outlet liquor (26% H ₃ PO ₄)	13.8 gm/l		2.93	100.8 gm/l
	505a/	Gypsum pond water	--	--	--	
	506	Reactor--granulator afterscrubber outlet liquor	1.7 gm/l			592.6 mg/l
	507	Cooler afterscrubber outlet liquor	1.8 gm/l			504.1 mg/l
	508b/	Drier afterscrubber outlet liquor	--			--
	509	Feed Acid (54% H ₃ PO ₄)	12.1 gm/l	850 gm/l		
	510	DAP product	26.4 mg/gm	520 mg/gm		211.2 mg/gm
2F	515.	Venturi scrubber inlet liquor (26% H ₃ PO ₄)	26.6 gm/l		0.033	
	516	Venturi scrubber outlet liquor (26% H ₃ PO ₄)	17.8 gm/l		1.78	86 gm/l
	517	Gypsum pond water	1.8 gm/l	2.7 gm/l	1.65	
	518	Reactor--granulator afterscrubber outlet liquor	1.7 gm/l			449.6 mg/l
	519	Cooler afterscrubber outlet liquor	1.9 gm/l			463.0 mg/l
	520	Drier afterscrubber outlet liquor	1.8 gm/l			828.0 mg/l
	521	Feed Acid (54% H ₃ PO ₄)	15.2 gm/l	800 gm/l		
	522	DAP product	26.0 mg/gm	470 mg/gm		197.5 mg/gm
3F	527	Venturi scrubber inlet liquor (26% H ₃ PO ₄)	25.6 gm/l		0.28	
	528	Venturi scrubber outlet liquor (26% H ₃ PO ₄)	6.0 gm/l		5.38	107.5 gm/l
	529	Gypsum pond water	2.0 gm/l	2.8 gm/l	1.75	
	530	Reactor--granulator afterscrubber outlet liquor	1.6 gm/l			487.1 mg/l
	531	Cooler afterscrubber outlet liquor	1.7 gm/l			1.3 gm/l
	532	Drier afterscrubber outlet liquor	1.7 gm/l			580 mg/l
	533	Feed Acid (54% H ₃ PO ₄)	14.5 gm/l	790 gm/l		
	534	DAP product	24.4 mg/gm	500 mg/gm		228.2 mg/gm
4F	537	Venturi scrubber inlet liquor (26% H ₃ PO ₄)	25.8 gm/l		0.37	
	538a/	Venturi scrubber outlet liquor (26% H ₃ PO ₄)	--		--	--
	539	Gypsum pond water	1.8 gm/l	2.8 gm/l	1.73	
	540	Farm runoff water	1.1 mg/l	14.5 mg/l	--	
	541	Reactor--granulator afterscrubber outlet liquor	1.7 gm/l			115.8 mg/l
	542	Cooler afterscrubber outlet liquor	1.8 gm/l			599.5 mg/l
	543	Drier afterscrubber outlet liquor	1.7 gm/l			1.3 gm/l
	544	Feed Acid (54% H ₃ PO ₄)	14.7 gm/l	750 gm/l		
	545	DAP product	26.0 mg/gm	480 mg/gm		201.0 mg/gm
5F	549	Venturi scrubber inlet liquor (26% H ₃ PO ₄)	27.5 gm/l		0.35	
	550	Venturi scrubber outlet liquor (26% H ₃ PO ₄)	7.2 gm/l		5.18	111.3 gm/l
	551	Gypsum pond water	1.8 gm/l	2.8 gm/l	1.73	
	552	Reactor--granulator afterscrubber outlet liquor	1.8 gm/l			910 mg/l
	553	Cooler afterscrubber outlet liquor	1.8 gm/l			630 mg/l
	554	Drier afterscrubber outlet liquor	1.7 gm/l			630 mg/l
	555	Feed Acid (54% H ₃ PO ₄)	15.5 gm/l	730 gm/l		
	556	DAP product	25.7 mg/gm	460 mg/gm		204.4 mg/gm

a/ Sample lost during shipment.

b/ Sample missing.

standard volume sampled, 44.135 DSCF and 0.3 mg NH₃, the concentration of ammonia is < 0.337 ppm.

Example Calculation

$$\text{Ave VMSTD} = 44.135 \text{ DSCF}$$

$$\text{Wt NH}_3 = < 0.3 \text{ mg}$$

$$\text{DSCF} \times 0.0283 = \text{NM}^3$$

$$\text{Mol. Wt NH}_3 = 17$$

$$\frac{0.3 \text{ mg}}{44.135 \times \text{DSCF} \times 0.0283 \text{ NM}^3/\text{DSCF}} = 0.2367 \text{ mg/NM}^3$$

$$\text{NM}^3 \times \frac{24.2}{\text{Mol. Wt}} = \text{ppm}$$

$$\frac{0.2367 \text{ mg/NM}^3 \times 24.2}{17} = < 0.337 \text{ ppm}$$

During the first fluoride run it was discovered that Point No. 3 in Port No. 2 was a dead spot. At first it was thought that the pitot tubes and lines were plugged. The test was stopped and the lines examined, but nothing was found. No ΔP reading was observed at this point. The project officer consulted with the ARCO people and they confirmed that they indeed had a dead spot in the stack. We moved an inch away and finished the run. On all future runs we stayed an inch away from Point No. 3 in Port No. 2.

On a process weight basis, the results of the five test runs range from 0.026 to 0.055 lb F/ton P_2O_5 and average 0.036 lb F/ton P_2O_5 .

In an attempt to compare the effectiveness of a spray-crossflow packed scrubber using fresh water with one using gypsum pond water, one of the five test runs was performed while one of the three packed scrubbers was using farm runoff water (not contaminated with fluorides) as the scrubbing liquor. Two such samples were to be taken, but due to process equipment failure, the collection of only one was possible. The result of this test run (Run No. 4) was 0.036 lb F/ton P_2O_5 . The average of many tests performed while one scrubber uses farm runoff water should be lower than the average of many tests performed while all the scrubbers are scrubbing with pond water contaminated with fluorides. The result of this single sample is not sufficient for a valid comparison and no conclusion can be made.

The sampling train for all five test runs was modified to include an unheated cyclone between the probe and the impingers. This modification was made in an attempt to indicate the relative amounts of pond water mist and/or other particulates in the sampled gas stream. The cyclone catches

contained from 0 to 0.013 lb F/ton P_2O_5 , which is from 0% to 35% of the total fluoride catches. Run No. 4 (using farm runoff water) yielded the highest value. If a significant quantity of fluoride contaminated mist is present in this plant's gas stream, the least amount of fluorides would be expected in the cyclone catch of Run No. 4. That this test did not yield the lowest percentage of fluorides captured in the cyclone, indicates that fluoride contaminated mist is not an appreciable portion of the total fluoride emissions at this plant.

Both changes, the sampling of the plant while one of the scrubbers was using farm runoff water and the inclusion of the cyclone in the sampling train, were attempts to show strong trends in the amount of particulates in the gas stream and the effect of scrubbing fluorides with fresh water. The results fail to indicate any strong trends. A complete analysis would require different methods and more samples.

III. PROCESS DESCRIPTION AND OPERATION

The diammonium phosphate (DAP) facility at ARCO Chemical Company, Fort Madison, Iowa, is designed to produce 750 tons/day of product (345 tons P_2O_5 /day). Normal operation is at the design rate.

At this location ammonia is reacted with phosphoric acid in a pre-neutralizer or reactor. Sulfuric acid is also added to the reaction mixture. The slurry from the reactor is fed to a granulator along with recycled off-size product and recovered dust. Additional ammonia is added in the granulator. From the granulator, the DAP product passes through a rotary

dryer. After drying, the product is screened to remove oversize and undersize product. The oversize product is ground in a cage mill and returned to the granulator along with the undersize fines. The on-size product is passed through a rotary cooler to storage.

Three separate systems are used to control the particulate, fluoride, and ammonia emissions from the process. The reactor-granulator system is equipped with a venturi scrubber followed by a crossflow packed scrubber of Teller design.

The dryer and cooler are each equipped with separate systems identical to the reactor-granulator control system, except that in each case, the venturi scrubber is preceded by a battery of four parallel cyclones for particulate removal.

Thirty percent acid, diluted to 25% with gypsum pond water, is used in each venturi scrubber to control fluorides and recover any ammonia in the gas stream. The spent scrubber liquor is returned to the process.

The packed scrubber serving the reactor-granulator can use either gypsum pond water containing 1,700 to 1,900 ppm fluoride as F (weight per volume), or farm runoff water with no fluoride content. The packed scrubbers serving the cooler and dryer use gypsum pond water as scrubbing liquor. A total of 130,000 to 150,000 SCFM are discharged from the three control systems through a common stack.

The first and second set of fluoride and ammonia samples were collected on 21 March 1973. The process operated at 100-110% of its design production rate, which is normal. The third and fourth sets of samples were

collected on 22 March 1973. During the first three tests, gypsum pond water was used in all three packed scrubbers to absorb fluorides. Prior to collection of the fourth sample, the reactor-granulator scrubber was switched to using farm runoff water, which is not contaminated with fluorides. The fifth and final set of samples was collected on 23 March 1973. These samples were programmed to be collected while the reactor-granulator packed scrubber was using farm runoff water. Collection of the sample began at 0939. At 0945, EPA was informed that there was a serious problem with the pump which delivers farm runoff water to the reactor-granulator scrubber. The scrubber was switched to using gypsum pond water at about 0948. The scrubbing water was switched almost instantaneously. There was no time when the scrubber was dry or operating at reduced water flow rates. Sampling was continued without interruption. Except for this one incident, the process and control systems were operating at normal and uniform conditions.

The ambient temperature during testing remained around 35°F. At this temperature, the moisture in the stack gases created a dense plume which continued for 50-75 ft beyond the stack and rendered visible emission measurements difficult. However, throughout all five tests runs, there were visible emissions which remained after the moisture plume dissipated. These emissions were estimated to be from 10-15% opacity.

IV. LOCATION OF SAMPLING PORTS

Figure 1 shows the location of the sampling ports in the North DAP stack at ARCO Chemical Company. There are four ports installed 90 degrees

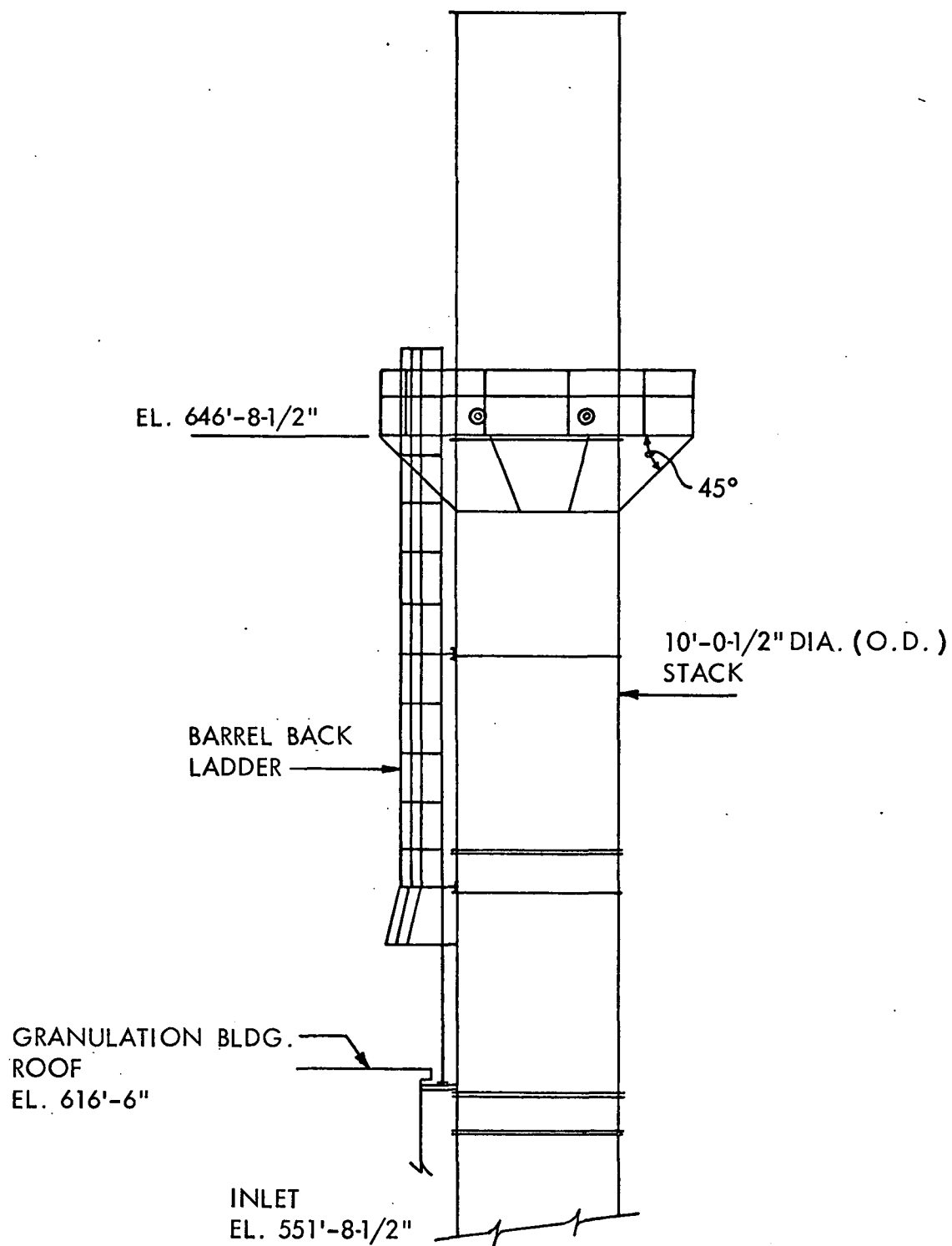


Figure 1 - DAP Plant Effluent Stack and Platform

apart at 8-1/2 pipe diameters from the upstream disturbance and 2-1/2 pipe diameters from the outlet. The fluoride samples were taken from three points in each port at distances of 5-1/4 in., 17-5/8 in., and 35-3/8 in., from the inside wall at each port.

The Orsat readings were obtained from integrated 30 min gas samples taken at a distance of 24 in. from the inside wall. The ammonia sampling was conducted at Point No. 3, Port No. 4 in the stack. Runs were of 1-hr duration.

During the fluoride emission tests, samples of scrubber feed, pond water makeup, scrubber outlet, feed acid and product, were taken. Figure 2 is a schematic, showing the location of the liquid samples taken. The product sample was obtained from the plant continuous composite sampler.

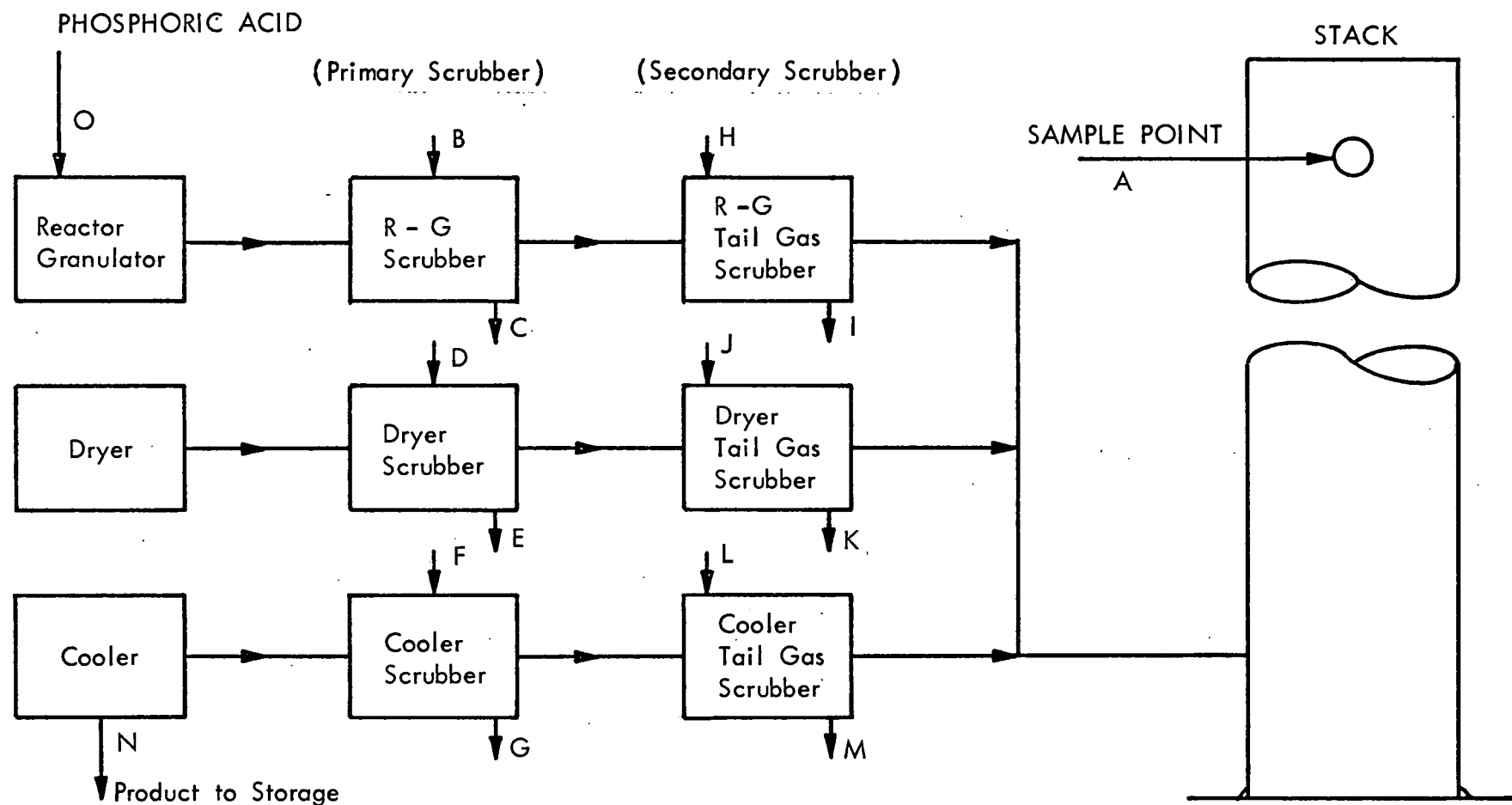
V. SAMPLING AND ANALYTICAL PROCEDURES

A. Fluorides

For the particulate fluoride sampling, the Research Appliance Company* Model 2343 "Staksamplr" equipment was used. The sampling train meets the specification of the Federal Register, 36, 17 August 1971, with one major change. The filter was installed between the third and last impinger instead of between the cyclone and first impinger, and No. 41 Whatman filter paper was used instead of the glass fiber filter. The analytical method used by the EPA Laboratory was the Spadns Zirconium Lake.^{1/}

* Mention of a specific company or product does not constitute endorsement by EPA.

^{1/} APHA-AWWA-WPCF, "Standard Methods for the Examination of Water and Wastewater," 13th Edition, 1971, pp. 174-176.



B, D, F - Primary Scrubber Feed-Composite (Approx. 25% Phosphoric Acid Solution)

H, J, L - Pond Water Make-Up-Composite

C, E, G - Primary Scrubber Outlet Discharge-Composite

I, K, M - Secondary Scrubber Outlet Discharge-Separate Samples

Figure 2 - Location of Liquid Samples

The network of sampling points has previously been described. The number of points on a traverse, sampling time at each point, and the sampling sequence were worked out in consultation with the EPA Field Officer. Preliminary measurements were made at the stack to determine temperature and velocity profiles. A moisture was assumed for the first test run, and calculated for the other tests from the moisture collected in the train on the previous run.

B. Ammonia

The ammonia sampling was conducted using the RAC* Model 2343 "Stak-samplr" equipment which meets the specification of the Federal Register, 36, 17 August 1971. There was one change: 100 ml of 30 g/liter H_2SO_4 was used in the first two impingers instead of 100 ml of water. The EPA laboratory used the Kjeldahl Distillation Analytical Method for ammonia.

C. Integrated Gas Samples

The equipment and procedure used for the collection of a cumulative or integrated gas sample are essentially the same as specified in the Federal Register. The gas sampling train, which deviates from the train design that is specified in the Register, is shown in Figure 3. This train design was approved by EPA prior to the test. The rate of sampling was controlled by adjusting a micrometer valve which acted as a critical orifice. The sampling

* Mention of a specific company or product does not constitute endorsement by EPA.

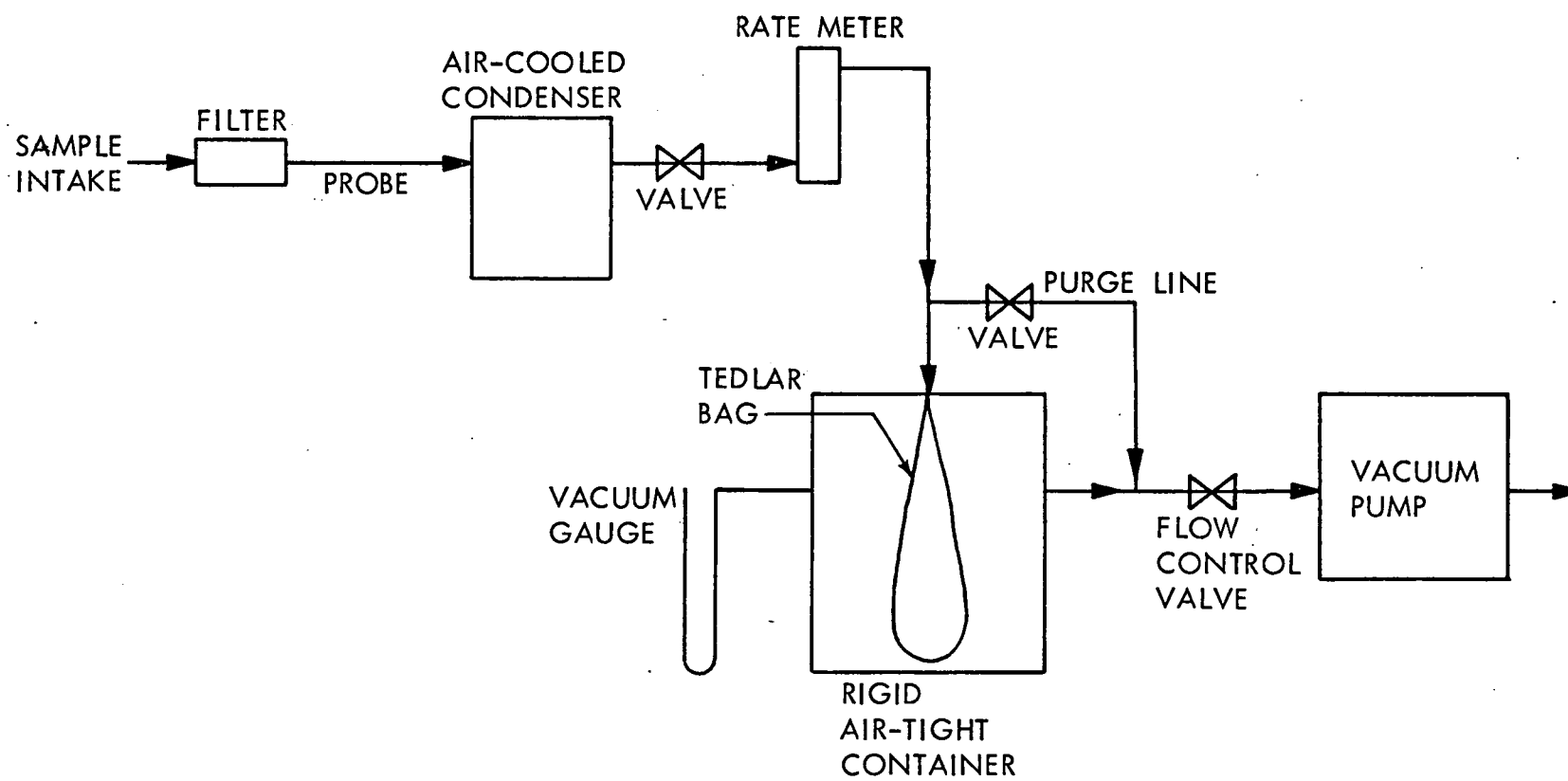


Figure 3 - Integrated Gas Sampling Train

rate was set at a constant value for any testing period, such that a total volume of gases between 1 and 1.5 cu ft were collected.

Analyses for carbon dioxide, oxygen, and carbon monoxide were performed in the field within a few hours after the sampling was completed, using an Orsat apparatus.

APPENDIX A

FLUORIDE RESULTS

This appendix contains Tables A-I through A-III. Table A-I shows the fluoride emission data for the total catch and cyclone catch. Table A-II is the sample calculations for fluoride total catch and cyclone catch. Table A-III contains the fluoride data and calculated values for the total catch and the cyclone catch.

TABLE A-I

FLUORIDE EMISSION DATA

NAME	DESCRIPTION	UNITS	1F	2F	3F	4F	5F
	DATE OF RUN		03-21-73	03-21-73	03-22-73	03-22-73	03-23-73
DN	PROBE TIP DIAMETER	IN	.250	.250	.250	.250	.250
TT	NET TIME OF RUN	MIN	120.0	120.0	120.0	120.0	120.0
PB	BAROMETRIC PRESSURE	IN.HG	29.80	29.78	29.72	29.60	29.80
PM	AVG ORIFICE PRES DROP	IN.H2O	.914	1.194	1.101	1.194	.897
VM	VOL DRY GAS-METER COND	DSCF	61.51	72.86	68.86	72.45	63.30
TM	AVG GAS METER TEMP	DEG.F	60.3	66.4	60.1	61.6	63.6
VMSTD	VOL DRY GAS-STD COND	DSCF	62.53	73.21	69.88	73.03	63.94
VW	TOTAL H2O COLLECTED	ML	91.3	109.9	102.4	87.9	109.1
VWV	VOL H2O VAPOR-STD COND	SCF	4.33	5.21	4.85	4.17	5.17
PMOS	PERCENT MOISTURE BY VOL		6.5	6.6	6.5	5.4	7.5
MD	MOLE FRACTION DRY GAS		.935	.934	.935	.946	.925
PCO2	PERCENT CO2 BY VOL, DRY		.3	.6	.2	.4	.2
PO2	PERCENT O2 BY VOL, DRY		20.5	21.0	20.2	20.6	20.6
PCO	PERCENT CO BY VOL, DRY		0.0	0.0	0.0	0.0	0.0
PN2	PERCENT N2 BY VOL, DRY		79.2	78.4	79.6	79.0	79.2
MWD	MOLECULAR WT-DRY STK GAS		28.86	28.94	28.84	28.89	28.86
MW	MOLECULAR WT-STK GAS		28.16	28.21	28.13	28.30	28.04
CP	PITOT TUBE COEFFICIENT		.850	.850	.850	.850	.850
DPS	AVG STK VELOCITY HEAD	IN.H2O	.320	.353	.300	.330	.247
TS	AVG STACK TEMPERATURE	DEG.F	112.0	111.9	114.3	107.3	110.7
NP	NET SAMPLING POINTS		24	24	24	24	24
PST	STATIC PRES OF STACK	IN.HG	.02	.03	.03	-.03	.03
PS	STACK PRESSURE, ABSOLUTE	IN.HG	29.82	29.81	29.75	29.57	29.83
VS	AVG STACK GAS VELOCITY	FPM	1991	2106	1923	2020	1728
AS	STACK AREA	IN2	11310	11310	11310	11310	11310
QS	STK FLOWRATE, DRY, STD CN	DSCFM	135060	142550	129498	138549	116248
QA	ACTUAL STACK FLOWRATE	ACFM	156408	165428	151009	158642	135750
PERI	PERCENT ISOKINETIC		88.6	98.3	103.2	100.9	105.3
B	ANISO CORRECTION FACTOR		1.000	1.000	1.000	1.000	1.000
MF	FLUORIDE WT-CYCLONE	MG	.50	.70	.10	.80	0.0
MT	FLUORIDE WT-TOTAL	MG	1.70	3.30	1.90	2.28	1.60
IC	PERC IMPINGER CATCH		71.4	78.8	95.7	64.9	100
CAN	FL. LOAD-PTL, STD CN	GR/DSCF	.00012	.00015	.00002	.00017	0.0
CAO	FL. LOAD-TTL, STD CN	GR/DSCF	.00042	.00070	.00042	.00048	.00039
CAT	FL. LOAD-PTL, STK CN	GR/ACF	.00011	.00013	.00002	.00015	0.0
CAU	FL. LOAD-TTL, STK CN	GR/ACF	.00036	.00060	.00036	.00042	.00033
CAW	FLUORIDE EMIS-PARTIAL	LB/HR	.14	.18	.02	.20	0.0
CAX	FLUORIDE EMIS-TOTAL	LB/HR	.49	.85	.47	.57	.39
	PROCESS FEED RATE	TON P ₂ O ₅ /HR	14.0	15.3	18.2	16.2	14.6
	EMISSIONS CYCLONE	LB F/TON P ₂ O ₅	.01	.0117	.001	.0123	0.0
	EMISSIONS TOTAL	LB F/TON P ₂ O ₅	.035	.0555	.0258	.0351	.0267

TABLE A-II

EXAMPLE FLUORIDE CALCULATIONS

1. VOLUME OF DRY GAS SAMPLED AT STANDARD CONDITIONS

$$\begin{aligned}
 VMSTD &= \frac{17.71 * VM * (PB + PM/13.6)}{TM + 460.} \\
 &= \frac{17.71 * 61.51 * (29.80 + .914/13.6)}{60.3 + 460.} = 62.53 \text{ DSCF}
 \end{aligned}$$

2. VOLUME OF WATER VAPOR AT STANDARD CONDITIONS

$$VWV = 0.0474 * VW = 0.0474 * 91.3 = 4.33 \text{ SCF}$$

3. PERCENT MOISTURE IN STACK GAS

$$\begin{aligned}
 PMOS &= \frac{100. * VWV}{VMSTD + VWV} = \frac{100. * 4.33}{62.53 + 4.33} = 6.5 \text{ PERCENT}
 \end{aligned}$$

4. MOLE FRACTION OF DRY STACK GAS

$$\begin{aligned}
 MD &= \frac{100. - PMOS}{100.} = \frac{100. - 6.5}{100.} = .935
 \end{aligned}$$

5. AVERAGE MOLECULAR WEIGHT OF DRY STACK GAS

$$\begin{aligned}
 MWD &= (PCO_2 * 44/100) + (PO_2 * 32/100) \\
 &\quad + (PN_2 + PCO * 28/100) \\
 &= (.3 * 44/100) + (20.5 * 32/100) \\
 &\quad + (79.2 * 28/100) \\
 &= 28.86
 \end{aligned}$$

6. MOLECULAR WEIGHT OF STACK GAS

$$\begin{aligned}
 MW &= MWD * MD + 18 * (1 - MD) \\
 &= 28.9 * .935 + 18 * (1 - .935) = 28.16
 \end{aligned}$$

TABLE A-II (Continued)

EXAMPLE FLUORIDE CALCULATIONS

7. STACK GAS VELOCITY AT STACK CONDITIONS

$$\begin{aligned} VS &= 4360 * \text{SQRT}(\text{DPS} * (\text{TS} + 460)) * \\ &\quad \text{SQRT}(1/(\text{PS} * \text{MW})) \\ &= 4360 * \text{SQRT}(.320 * (112.0 + 460)) \\ &\quad * \text{SQRT}(1/(29.82 * 28.16)) = 1991 \text{ FPM} \end{aligned}$$

8. STACK GAS VOLUMETRIC FLOW AT STANDARD CONDITIONS, DRY BASIS

$$\begin{aligned} QS &= \frac{0.123 * VS * AS * MD * PS}{\text{TS} + 460} \\ &= \frac{0.123 * 1991 * 11310 * .935 * 29.82}{112.0 + 460} = 135060 \text{ DSCFM} \end{aligned}$$

9. STACK GAS VOLUMETRIC FLOW AT STACK CONDITIONS

$$\begin{aligned} QA &= \frac{QS * (\text{TS} + 460)}{17.71 * PS * MD} \\ &= \frac{135060 * (112.0 + 460)}{17.71 * 29.82 * .935} = 156408 \text{ ACFM} \end{aligned}$$

10. PERCENT ISOKINETIC AND ANISO CORRECTION FACTOR

$$\begin{aligned} \text{PERI} &= \frac{1032 * (\text{TS} + 460) * \text{VMSTD}}{VS * \text{TT} * PS * MD * (\text{DN} * \text{DN})} \\ &= \frac{1032 * (112.0 + 460) * 62.53}{1991 * 120.0 * 29.82 * .935 * .250 * .250} = 88.6 \text{ PERCENT} \\ B &= 1.000 \end{aligned}$$

TABLE A-II (Continued)

EXAMPLE FLUORIDE CALCULATIONS

11. FLUORIDE LOADING -- PROBE, CYCLONE, AND FILTER
(AT STANDARD CONDITIONS)

$$CAN = 0.0154 * (MF/VMSTD) * B$$

$$= 0.0154 * (.50 / 62.53) * 1.000 = .00012 \text{ GR/DSCF}$$

12. FLUORIDE LOADING -- TOTAL (AT
STANDARD CONDITIONS)

$$CAO = 0.0154 * (MT/VMSTD) * B$$

$$= 0.0154 * (1.70 / 62.53) * 1.000 = .00042 \text{ GR/DSCF}$$

13. FLUORIDE LOADING -- PROBE, CYCLONE, AND FILTER
(AT STACK CONDITIONS)

$$CAT = \frac{17.71 * CAN * PS * MD}{TS + 460}$$

$$= \frac{17.71 * .0001 * 29.82 * .935}{112.0 + 460} = .00011 \text{ GR/ACF}$$

14. FLUORIDE LOADING -- TOTAL (AT
STACK CONDITIONS)

$$CAU = \frac{17.71 * CAO * PS * MD}{TS + 460}$$

$$= \frac{17.71 * .0004 * 29.82 * .935}{112.0 + 460} = .00036 \text{ GR/ACF}$$

TABLE A-II (Concluded)

EXAMPLE FLUORIDE CALCULATIONS

15. FLUORIDE EMISSION RATE

-- PROBE, CYCLONE, AND FILTER

$$CAW = 0.00857 * CAN * QS$$

$$= 0.00857 * .0001 * 135060 = .14 \text{ LB/HR}$$

16. FLUORIDE EMISSION RATE

-- TOTAL

$$CAX = 0.00857 * CAO * QS$$

$$= 0.00857 * .0004 * 135060 = .49 \text{ LB/HR}$$

TABLE A-III

FLUORIDE DATA AND CALCULATED VALUES

RUN- 1F DATE- 03-21-73

ATMOS TEMP (DG.F)	ATMOS PRES (I.HG)	STACK VAC (I.H2O)	H2O COND (ML)	FLUORIDE WT-SOL (MG)	FLUORIDE WT-TTL (MG)	STACK AREA (FT2)	INIT VOL (DCF)	PERC O2 DRY	PERC CO2 DRY	PERC CO DRY	PITOT TUBE COEF
43.0	29.80	-.29	91.3	1.70	1.70	78.54	5.31	20.5	.3	0.0	.850
CYCLONE CATCH				.50	.50						

PORT- POINT	SAMP TIME (MIN)	METER VOL (DCF)	DELTA P (I.H2O)	DELTA H (I.H2O)	TEMP IN (D.F)	TEMP OUT (D.F)	TRAIN VAC (I.HG)	STACK TEMP (D.F)	BOX TEMP (D.F)	PROBE T DIA (IN)	VEL (FPM)
1	1	5.00	7.50	.240	.660	50.0	49.0	5.0	105.0		.250 1751.3
1	1	5.00	9.77	.240	.660	54.0	50.0	3.0	105.0		.250 1751.3
1	2	5.00	11.54	.240	.660	55.0	50.0	3.0	105.0		.250 1751.3
1	2	5.00	13.38	.200	.520	57.0	53.0	5.0	107.0		.250 1601.6
1	3	5.00	15.82	.200	.570	59.0	54.0	5.0	106.0		.250 1600.1
1	3	5.00	18.41	.300	.850	61.0	55.0	5.0	107.0	75.0	.250 1961.5
2	1	5.00	20.81	.300	.850	55.0	55.0	5.0	107.0		.250 1961.5
2	3	5.00	23.26	.260	.740	62.0	56.0	5.0	107.0		.250 1826.1
2	2	5.00	25.69	.260	.740	65.0	57.0	5.0	108.0		.250 1827.7
2	2	5.00	28.14	.260	.740	68.0	58.0	5.0	108.0		.250 1827.7
2	3	5.00	29.56	.070	.210	56.0	58.0	3.0	108.0		.250 948.3
2	3	5.00	30.85	.070	.210	58.0	59.0	3.0	109.0		.250 949.2
3	1	5.00	33.55	.390	1.100	60.0	57.0	6.0	115.0		.250 2252.2
3	1	5.00	36.36	.390	1.100	63.0	58.0	6.5	115.0		.250 2252.2
3	2	5.00	39.33	.450	1.280	67.0	58.0	7.5	120.0		.250 2429.7
3	2	5.00	42.42	.460	1.300	69.0	59.0	7.0	120.0	65.0	.250 2456.6
3	3	5.00	45.55	.450	1.280	72.0	60.0	8.0	118.0		.250 2425.5
3	3	5.00	48.81	.490	1.390	74.0	61.0	8.0	118.0		.250 2531.0
4	1	5.00	51.50	.350	1.000	60.0	59.0	6.5	112.0	65.0	.250 2128.0
4	1	5.00	54.28	.410	1.200	65.0	60.0	7.0	111.0		.250 2301.2
4	2	5.00	57.36	.410	1.200	71.0	60.0	8.0	112.0		.250 2303.2
4	2	5.00	60.55	.410	1.200	72.0	62.0	8.0	112.0		.250 2303.2
4	3	5.00	63.63	.410	1.200	74.0	62.0	8.0	119.0		.250 2317.2
4	3	5.00	66.82	.420	1.280	74.0	63.0	8.0	115.0		.250 2337.2

TABLE A-III (Continued)
FLUORIDE DATA AND CALCULATED VALUES

RUN- 2F DATE- 03-21-73

ATMOS TEMP (DG.F)	ATMOS PRES (I.HG)	STACK VAC (I.H2O)	H2O COND (ML)	FLUORIDE WT-SOL (MG)	FLUORIDE WT-TTL (MG)	STACK AREA (FT2)	INIT VOL (DCF)	PERC O2 DRY	PERC CO2 DRY	PERC CO DRY	PITOT TUBE COEF
50.0	29.78	-.35	109.9	3.30	3.30	78.54	66.88	21.0	.6	0.0	.850

CYCLONE CATCH

.70 .70

PORT- POINT	SAMP TIME (MIN)	METER VOL (DCF)	DELTA P (I.H2O)	DELTA H (I.H2O)	TEMP IN (D.F)	TEMP OUT (D.F)	TRAIN VAC (I.HG)	STACK TEMP (D.F)	BOX TEMP (D.F)	PROBE T DIA (IN)	VEL (FPM)
1	1	5.00	69.65	.350	1.020	54.0	53.0	4.0	110.0	.250	2122.9
1	1	5.00	72.46	.350	1.020	59.0	54.0	4.0	110.0	.250	2122.9
1	2	5.00	75.34	.380	1.120	67.0	55.0	4.0	109.0	.250	2210.1
1	2	5.00	78.56	.410	1.220	72.0	57.0	4.0	109.0	82.0	.250 2295.7
1	3	5.00	81.30	.330	1.000	75.0	59.0	4.0	120.0	.250	2079.4
1	3	5.00	84.12	.330	1.000	76.0	61.0	4.0	120.0	.250	2079.4
2	1	5.00	86.85	.280	.970	67.0	62.0	4.0	125.0	.250	1923.6
2	1	5.00	89.75	.320	1.060	70.0	63.0	4.0	125.0	95.0	.250 2056.4
2	2	5.00	92.46	.270	.950	76.0	64.0	4.0	125.0	.250	1889.0
2	2	5.00	95.24	.270	.950	78.0	64.0	4.0	125.0	.250	1889.0
2	3	5.00	97.30	.090	.320	76.0	66.0	2.0	122.0	.250	1087.8
2	3	5.00	98.99	.090	.320	74.0	66.0	2.0	122.0	.250	1087.8
3	1	5.00	102.28	.405	1.450	65.0	65.0	5.0	120.0	69.0	.250 2303.6
3	1	5.00	105.70	.405	1.450	70.0	64.0	5.5	110.0	.250	2283.7
3	2	5.00	109.20	.460	1.600	76.0	64.0	6.0	109.0	.250	2431.6
3	2	5.00	112.80	.460	1.600	80.0	65.0	6.0	109.0	61.0	.250 2431.6
3	3	5.00	116.34	.480	1.700	80.0	66.0	6.0	109.0	.250	2483.9
3	3	5.00	119.92	.480	1.700	81.0	66.0	6.0	108.0	.250	2481.8
4	1	5.00	123.15	.350	1.250	67.0	44.0	5.0	109.0	.250	2121.1
4	1	5.00	126.36	.350	1.250	70.0	63.0	5.0	105.0	.250	2113.6
4	2	5.00	129.74	.410	1.450	71.0	63.0	5.5	101.0	55.0	.250 2279.5
4	2	5.00	133.12	.410	1.450	72.0	63.0	6.0	100.0	.250	2277.5
4	3	5.00	136.45	.400	1.400	72.0	62.0	5.5	100.0	.250	2249.5
4	3	5.00	139.74	.400	1.400	70.0	62.0	5.5	100.0	.250	2249.5

TABLE A-III (Continued)
FLUORIDE DATA AND CALCULATED VALUES

RUN- 3F DATE- 03-22-73

ATMOS TEMP (DG.F)	ATMOS PRES (I.HG)	STACK VAC (I.H2O)	H2O COND (ML)	FLUORIDE WT-SOL (MG)	FLUORIDE WT-TTL (MG)	STACK AREA (FT2)	INIT VOL (DCF)	PERC O2 DRY	PERC CO2 DRY	PERC CO DRY	PITOT TUBE COEF
45.0	29.72	-.35	102.4	1.90	1.90	78.54	140.12	20.2	.2	0.0	.850

CYCLONE CATCH .10 .10

PORT- POINT	SAMP TIME (MIN)	METER VOL (DCF)	DELTA P (I.H2O)	DELTA H (I.H2O)	TEMP IN (D.F)	TEMP OUT (D.F)	TRAIN VAC (I.HG)	STACK TEMP (D.F)	BOX TEMP (D.F)	PROBE T DIA (IN)	VEL (FPM)
1	1	5.00	142.98	.230	.750	48.0	48.0	5.0	109.0		.250 1723.4
1	1	5.00	145.40	.230	.750	54.0	50.0	5.0	110.0	50.0	.250 1724.9
1	2	5.00	148.20	.290	1.020	55.0	50.0	6.0	110.0		.250 1936.9
1	2	5.00	151.08	.310	1.110	59.0	51.0	7.0	108.0		.250 1999.1
1	3	5.00	153.78	.250	.910	58.0	52.0	6.0	109.0		.250 1796.8
1	3	5.00	156.48	.260	.920	60.0	52.0	6.0	108.0		.250 1830.8
2	1	5.00	159.03	.240	.870	50.0	52.0	5.0	106.0		.250 1755.9
2	1	5.00	161.58	.230	.800	56.0	52.0	5.0	106.0		.250 1718.9
2	2	5.00	163.86	.190	.660	60.0	53.0	4.0	108.0		.250 1565.0
2	2	5.00	166.22	.200	.690	62.0	54.0	4.0	110.0		.250 1608.5
2	3	5.00	167.48	.030	.100	61.0	55.0	2.0	114.0		.250 625.2
2	3	5.00	168.45	.030	.100	60.0	56.0	2.0	113.0	50.0	.250 624.6
3	1	5.00	171.79	.360	1.350	57.0	56.0	8.0	115.0		.250 2167.5
3	1	5.00	174.93	.360	1.350	65.0	57.0	8.0	116.0	50.0	.250 2169.4
3	2	5.00	178.35	.410	1.570	71.0	59.0	8.0	116.0		.250 2315.1
3	2	5.00	181.81	.410	1.570	74.0	60.0	8.5	115.0		.250 2313.1
3	3	5.00	185.31	.450	1.700	77.0	62.0	10.0	117.0		.250 2427.6
3	3	5.00	188.97	.450	1.700	79.0	62.0	10.0	115.0		.250 2423.3
4	1	5.00	192.20	.340	1.250	60.0	62.0	8.5	125.0	50.0	.250 2124.7
4	1	5.00	195.45	.340	1.250	68.0	62.0	9.0	120.0		.250 2115.6
4	2	5.00	198.80	.390	1.450	70.0	62.0	9.0	118.0		.250 2261.9
4	2	5.00	202.17	.400	1.500	72.0	62.0	9.0	119.0		.250 2292.7
4	3	5.00	205.57	.400	1.500	75.0	63.0	9.5	121.0	50.0	.250 2296.6
4	3	5.00	208.98	.410	1.550	76.0	64.0	9.5	122.0		.250 2327.2

TABLE A-III (Continued)
FLUORIDE DATA AND CALCULATED VALUES

RUN- 4F DATE- 03-22-73

ATMOS TEMP (DG.F)	ATMOS PRES (I.HG)	STACK VAC (I.H2O)	H2O COND (ML)	FLUORIDE WT-SOL (MG)	FLUORIDE WT-TTL (MG)	STACK AREA (FT2)	INIT VOL (DCF)	PERC O2 DRY	PERC CO2 DRY	PERC CO DRY	PITOT TUBE COEF
54.0	29.60	.35	87.9	2.20	2.28	78.54	209.09	20.6	.4	0.0	.850

CYCLONE CATCH .80 .80

PORT- POINT	SAMP TIME (MIN)	METER VOL (DCF)	DELTA P (I.H2O)	DELTA H (I.H2O)	TEMP IN (D.F)	TEMP OUT (D.F)	TRAIN VAC (I.HG)	STACK TEMP (D.F)	BOX TEMP (D.F)	PROBE T DIA (IN)	VEL (FPM)
1	1	5.00	.250	.930	54.0	54.0	5.0	105.0		.250	1790.4
1	1	5.00	.270	1.000	59.0	55.0	5.0	103.0		.250	1857.4
1	2	5.00	.360	1.310	66.0	56.0	5.0	105.0		.250	2148.5
1	2	5.00	.360	1.310	68.0	57.0	5.0	105.0		.250	2148.5
1	3	5.00	.330	1.210	68.0	58.0	5.0	106.0		.250	2058.8
1	3	5.00	.310	1.180	66.0	58.0	5.0	106.0		.250	1995.5
2	1	5.00	.300	1.120	58.0	58.0	4.5	108.0		.250	1966.5
2	1	5.00	.300	1.120	64.0	58.0	4.5	116.0		.250	1980.3
2	2	5.00	.220	.790	67.0	60.0	3.5	117.0	50.0	.250	1697.3
2	2	5.00	.210	.750	67.0	60.0	3.5	117.0		.250	1658.3
2	3	5.00	.060	.220	64.0	61.0	1.0	117.0		.250	886.4
2	3	5.00	.050	.185	62.0	61.0	1.0	110.0		.250	804.2
3	1	5.00	.360	1.290	56.0	58.0	5.0	110.0		.250	2158.0
3	1	5.00	.360	1.290	61.0	59.0	5.0	107.0		.250	2152.3
3	2	5.00	.420	1.500	66.0	59.0	5.5	106.0		.250	2322.7
3	2	5.00	.420	1.500	68.0	60.0	5.5	106.0		.250	2322.7
3	3	5.00	.450	1.600	69.0	60.0	6.0	103.0		.250	2397.8
3	3	5.00	.460	1.630	69.0	60.0	6.0	103.0		.250	2424.3
4	1	5.00	.360	1.300	60.0	59.0	5.0	105.0		.250	2148.5
4	1	5.00	.380	1.350	64.0	60.0	5.0	108.0		.250	2213.2
4	2	5.00	.420	1.500	66.0	60.0	5.5	107.0		.250	2324.7
4	2	5.00	.420	1.500	69.0	60.0	5.5	107.0		.250	2324.7
4	3	5.00	.430	1.530	67.0	60.0	6.0	105.0	50.0	.250	2348.1
4	3	5.00	.430	1.530	66.0	60.0	6.0	105.0		.250	2348.1

TABLE A-III (Concluded)

FLUORIDE DATA AND CALCULATED VALUES

RUN- 5F DATE- 03-23-73

ATMOS TEMP (DG.F)	ATMOS PRES (I.HG)	STACK VAC (I.H2O)	H2O COND (ML)	FLUORIDE WT-SOL (MG)	FLUORIDE WT-TTL (MG)	STACK AREA (FT2)	INIT VOL (DCF)	PERC O2 DRY	PERC CO2 DRY	PERC CO DRY	PITOT TUBE COEF
52.0	29.80	-.39	109.1	1.60	1.60	78.54	281.65	20.6	.2	0.0	.850

CYCLONE CATCH

0.0

0.0

PORT- POINT	SAMP TIME (MIN)	METER VOL (DCF)	DELTA P (I.H2O)	DELTA H (I.H2O)	TEMP IN (D.F)	TEMP OUT (D.F)	TRAIN VAC (I.HG)	STACK TEMP (D.F)	BOX TEMP (D.F)	PROBE T DIA (IN)	VEL (FPM)
1	1	5.00	283.94	.190	.685	53.0	54.0	4.0	109.0	.250	1566.8
1	1	5.00	286.32	.190	.685	56.0	54.0	5.0	110.0	.250	1568.2
1	2	5.00	289.03	.260	.930	60.0	55.0	5.0	110.0	.250	1834.4
1	2	5.00	291.80	.270	.960	61.0	56.0	5.0	109.0	.250	1867.7
1	3	5.00	294.41	.230	.830	64.0	57.0	5.2	107.0	.250	1720.8
1	3	5.00	297.03	.220	.780	64.0	58.0	5.5	110.0	.250	1687.4
2	1	5.00	299.50	.210	.750	58.0	58.0	5.0	108.0	50.0	.250 1645.7
2	1	5.00	302.00	.210	.750	61.0	59.0	5.0	110.0	.250	1648.6
2	2	5.00	304.24	.150	.570	64.0	60.0	4.0	110.0	.250	1393.4
2	2	5.00	306.44	.150	.570	66.0	60.0	4.0	110.0	.250	1393.4
2	3	5.00	307.73	.010	.110	63.0	61.0	2.0	110.0	.250	359.8
2	3	5.00	308.83	.010	.110	63.0	62.0	2.0	110.0	.250	359.8
3	1	5.00	311.64	.280	1.000	62.0	62.0	6.0	112.0	.250	1907.0
3	1	5.00	314.48	.280	1.000	68.0	63.0	6.0	112.0	.250	1907.0
3	2	5.00	317.55	.340	1.210	70.0	64.0	7.0	112.0	.250	2101.4
3	2	5.00	320.65	.330	1.180	72.0	65.0	7.0	112.0	.250	2070.3
3	3	5.00	323.71	.360	1.300	76.0	66.0	8.0	112.0	.250	2162.4
3	3	5.00	326.80	.360	1.300	76.0	67.0	8.0	110.0	.250	2158.6
4	1	5.00	329.91	.290	1.050	64.0	65.0	7.0	110.0	.250	1937.4
4	1	5.00	332.87	.290	1.050	68.0	65.0	7.0	112.0	.250	1940.8
4	2	5.00	335.90	.330	1.200	72.0	65.0	8.0	110.0	.250	2066.7
4	2	5.00	338.95	.330	1.200	72.0	66.0	8.0	110.0	.250	2066.7
4	3	5.00	341.95	.330	1.180	73.0	66.0	7.0	115.0	60.0	.250 2075.7
4	3	5.00	344.95	.320	1.120	73.0	66.0	7.0	114.0	60.0	.250 2042.2

APPENDIX B

GASEOUS RESULTS

Tables B-I, B-II, and B-III contain the results of the testing for ammonia in the stack gas from the DAP plant. Table B-I contains the summary of results, and Table B-II contains the ammonia emission data. Table B-III contains the ammonia data and calculated values.

The results of the moisture and Orsat analysis are presented in Section III of this report.

TABLE B-I

SUMMARY OF RESULTS - AMMONIA

NAME	DESCRIPTION	UNITS	1-NH3	2-NH3	3-NH3	4-NH3
	DATE OF RUN		03-21-73	03-21-73	03-22-73	03-23-73
QS	STK FLOWRATE, DRY, STD CN	DSCFM	149763	166169	162765	151092
QA	ACTUAL STACK FLOWRATE	ACFM	170816	188266	184013	171879
PMOS	PERCENT MOISTURE BY VOL		7.0	6.7	6.4	7.5
PCO2	PERCENT CO2 BY VOL, DRY		.3	.6	.2	.2
P02	PERCENT O2 BY VOL, DRY		20.5	21.0	20.2	20.6
PCO	PERCENT CO BY VOL, DRY		0.0	0.0	0.0	0.0

AMMONIA -- TOTAL CATCH

MT	AMMONIA WT-TOTAL	MG	< .30	< .30	< .30	< .30
CAO	AMMONIA LOAD-TTL, STD CN	GR/DSCF				
CAU	AMMONIA LOAD-TTL, STK CN	GR/ACF				
CAX	AMMONIA EMIS-TOTAL	LB/HR				

DATE OF OUTPUT 07-13-73

PROGRAM DATE 01-31-72

TABLE B-II

AMMONIA EMISSION DATA

NAME	DESCRIPTION	UNITS	1-NH3	2-NH3	3-NH3	4-NH3
	DATE OF RUN		03-21-73	03-21-73	03-22-73	03-23-73
DN	PROBE TIP DIAMETER	IN	.250	.250	.250	.250
TT	NET TIME OF RUN	MIN	60.0	60.0	60.0	60.0
PB	BAROMETRIC PRESSURE	IN.HG	29.80	29.87	29.72	29.80
PM	AVG ORIFICE PRES DROP	IN.H2O	1.844	1.845	1.840	1.840
VM	VOL DRY GAS-METER COND	DCF	43.79	43.67	44.93	42.68
TM	AVG GAS METER TEMP	DEG.F	62.1	73.0	62.5	65.3
VMSTD	VOL DRY GAS-STD COND	DSCF	44.46	43.54	45.46	43.08
VW	TOTAL H2O COLLECTED	ML	70.5	65.7	65.8	73.2
VWV	VOL H2O VAPOR-STD COND	SCF	3.34	3.11	3.12	3.47
PMOS	PERCENT MOISTURE BY VOL		7.0	6.7	6.4	7.5
MD	MOLE FRACTION DRY GAS		.930	.933	.936	.925
PCO2	PERCENT CO2 BY VOL, DRY		.3	.6	.2	.2
PO2	PERCENT O2 BY VOL, DRY		20.5	21.0	20.2	20.6
PCO	PERCENT CO BY VOL, DRY		0.0	0.0	0.0	0.0
PN2	PERCENT N2 BY VOL, DRY		79.2	78.4	79.6	79.2
MWD	MOLECULAR WT-DRY STK GAS		28.86	28.94	28.84	28.86
MW	MOLECULAR WT-STK GAS		28.10	28.20	28.14	28.05
CP	PITOT TUBE COEFFICIENT		.850	.850	.850	.850
DPS	AVG STK VELOCITY HEAD	IN.H2O	.372	.456	.434	.382
TS	AVG STACK TEMPERATURE	DEG.F	99.8	99.7	97.3	96.0
NP	NET SAMPLING POINTS		12	12	12	12
PST	STATIC PRES OF STACK	IN.HG	-0.00	.03	.03	.03
PS	STACK PRESSURE, ABSOLUTE	IN.HG	29.80	29.90	29.75	29.83
VS	AVG STACK GAS VELOCITY	FPM	2175	2397	2343	2188
AS	STACK AREA	IN2	11310	11310	11310	11310
QS	STK FLOWRATE, DRY, STD CN	DSCFM	149763	166169	162765	151092
QA	ACTUAL STACK FLOWRATE	ACFM	170816	188266	184013	171879
PERI	PERCENT ISOKINETIC		113.6	100.2	106.8	109.0
B	ANISO CORRECTION FACTOR		1.000	1.000	1.000	1.000

TABLE B-III

AMMONIA DATA AND CALCULATED VALUES

RUN- 1-NH3 DATE- 03-21-73

ATMOS TEMP (DG.F)	ATMOS PRES (I.HG)	STACK VAC (I.H2O)	H2O COND (ML)	PARTIC WT-PTL (MG)	PARTIC WT-TTL (MG)	STACK AREA (FT2)	INIT VOL (DCF)	PERC O2 DRY	PERC CO2 DRY	PERC CO DRY	PITOT TUBE COEF
43.0	29.80	0.00	70.5	< .30	< .30	78.54	936.05	20.5	.3	0.0	.850

PORT- POINT	SAMP TIME (MIN)	METER VOL (DCF)	DELTA P (I.H2O)	DELTA H (I.H2O)	TEMP IN (D.F)	TEMP OUT (D.F)	TRAIN VAC (I.HG)	STACK TEMP (D.F)	BOX TEMP (D.F)	PROBE T DIA (IN)	VEL (FPM)
	5.00	939.54	.365	1.840	55.0	51.0	8.5	105.0	50.0	.250	2162.7
	5.00	943.35	.370	1.840	58.0	51.0	8.5	102.0	52.0	.250	2171.7
	5.00	947.30	.360	1.840	63.0	53.0	8.0	100.0		.250	2138.3
	5.00	951.06	.370	1.840	68.0	54.0	7.0	96.0		.250	2160.1
	5.00	954.03	.375	1.840	70.0	56.0	7.0	96.0		.250	2174.6
	5.00	958.38	.380	1.850	70.0	57.0	7.0	95.0		.250	2187.1
	5.00	961.09	.370	1.850	70.0	57.0	7.0	98.0		.250	2163.9
	5.00	965.51	.370	1.840	71.0	59.0	7.5	94.0		.250	2156.2
	5.00	969.41	.370	1.840	71.0	59.0	8.0	100.0		.250	2167.8
	5.00	972.72	.380	1.900	72.0	60.0	9.0	106.0		.250	2208.7
	5.00	976.26	.380	1.850	72.0	60.0	10.0	106.0		.250	2208.7
	5.00	979.84	.380	1.800	73.0	61.0	13.0	101.0		.250	2198.9

TABLE B-III (Continued)

AMMONIA DATA AND CALCULATED VALUES

RUN- 2-NH3 DATE- 03-21-73

ATMOS TEMP (DG.F)	ATMOS PRES (I.HG)	STACK VAC (I.H2O)	H2O COND (ML)	PARTIC WT-PTL (MG)	PARTIC WT-TTL (MG)	STACK AREA (FT2)	INIT VOL (DCF)	PERC O2 DRY	PERC CO2 DRY	PERC CO DRY	PITOT TUBE COEF
50.0	29.87	-.35	65.7	< .30	< .30	78.54	980.68	21.0	.6	0.0	.850

33

PORT- POINT	SAMP TIME (MIN)	METER VOL (DCF)	DELTA P (I.H2O)	DELTA H (I.H2O)	TEMP IN (D.F)	TEMP OUT (D.F)	TRAIN VAC (I.HG)	STACK TEMP (D.F)	BOX TEMP (D.F)	PROBE T DIA (IN)	VEL (FPM)
3 1	5.00	984.22	.500	1.840	57.0	54.0	5.0	98.0		.250	2507.0
	5.00	987.90	.460	1.840	65.0	55.0	5.0	98.0		.250	2404.6
	5.00	991.39	.450	1.840	74.0	57.0	5.5	99.0	50.0	.250	2380.4
	5.00	995.03	.460	1.840	80.0	60.0	6.0	99.0	50.0	.250	2406.7
	5.00	998.60	.460	1.840	84.0	62.0	6.0	100.0		.250	2408.9
	5.00	1002.37	.460	1.840	87.0	63.0	6.0	100.0		.250	2408.9
	5.00	1005.95	.450	1.840	88.0	66.0	6.5	100.0		.250	2382.6
	5.00	1009.60	.450	1.840	88.0	66.0	7.0	100.0		.250	2382.6
	5.00	1013.31	.450	1.840	90.0	67.0	7.0	100.0		.250	2382.6
	5.00	1017.02	.450	1.840	93.0	68.0	7.5	101.0		.250	2384.7
	5.00	1020.67	.440	1.840	94.0	70.0	8.0	101.0		.250	2358.0
	5.00	1024.35	.440	1.900	93.0	70.0	10.0	101.0		.250	2358.0

TABLE B-III (Continued)

AMMONIA DATA AND CALCULATED VALUES

RUN- 3-NH3 DATE- 03-22-73

ATMOS TEMP (DG.F)	ATMOS PRES (I.HG)	STACK VAC (I.H2O)	H2O COND (ML)	PARTIC WT-PTL (MG)	PARTIC WT-TTL (MG)	STACK AREA (FT2)	INIT VOL (DCF)	PERC O2 DRY	PERC CO2 DRY	PERC CO DRY	PITOT TUBE COEF
45.0	29.72	-.35	65.8	< .30	< .30	78.54	24.80	20.2	.2	0.0	.850

34

PORT- POINT	SAMP TIME (MIN)	METER VOL (DCF)	DELTA P (I.H2O)	DELTA H (I.H2O)	TEMP IN (D.F)	TEMP OUT (D.F)	TRAIN VAC (I.HG)	STACK TEMP (D.F)	BOX TEMP (D.F)	PROBE T DIA (IN)	VEL (FPM)
3 1	5.00	28.55	.430	1.840	50.0	45.0	8.0	97.0		.250	2331.2
	5.00	32.19	.430	1.840	60.0	48.0	8.0	97.0		.250	2331.2
	5.00	35.85	.430	1.840	66.0	50.0	9.0	97.0		.250	2331.2
	5.00	39.58	.430	1.840	69.0	52.0	9.0	98.0		.250	2333.3
	5.00	43.35	.430	1.840	72.0	53.0	9.0	95.0		.250	2327.0
	5.00	47.10	.430	1.840	73.0	55.0	9.0	95.0	50.0	.250	2327.0
	5.00	50.80	.430	1.840	75.0	56.0	9.0	95.0		.250	2327.0
	5.00	54.57	.430	1.840	76.0	57.0	9.0	95.0		.250	2327.0
	5.00	58.32	.440	1.840	76.0	58.0	9.0	100.0		.250	2364.5
	5.00	62.09	.440	1.840	76.0	58.0	9.5	101.0		.250	2366.6
	5.00	65.89	.440	1.840	78.0	60.0	10.0	99.0		.250	2362.4
	5.00	69.73	.450	1.840	78.0	60.0	10.5	98.0		.250	2386.9

TABLE B-III (Concluded)

AMMONIA DATA AND CALCULATED VALUES

RUN- 4-NH3 DATE- 03-23-73

ATMOS TEMP (DG.F)	ATMOS PRES (I.HG)	STACK VAC (I.H2O)	H2O COND (ML)	PARTIC WT-PTL (MG)	PARTIC WT-TTL (MG)	STACK AREA (FT2)	INIT VOL (DCF)	PERC O2 DRY	PERC CO2 DRY	PERC CO DRY	PITOT TUBE COEF
52.0	29.80	-.35	73.2	< .30	< .30	78.54	69.81	20.6	.2	0.0	.850

35

PORT- POINT	SAMP TIME (MIN)	METER VOL (DCF)	DELTA P (I.H2O)	DELTA H (I.H2O)	TEMP IN (D.F)	TEMP OUT (D.F)	TRAIN VAC (I.HG)	STACK TEMP (D.F)	BOX TEMP (D.F)	PROBE T DIA (IN)	VEL (FPM)
4	5.00	73.24	.380	1.840	61.0	54.0	8.0	100.0		.250	2198.2
	5.00	76.88	.380	1.840	66.0	55.0	7.7	100.0		.250	2198.2
	5.00	80.34	.380	1.840	68.0	56.0	7.7	98.0		.250	2194.3
	5.00	83.86	.375	1.840	70.0	57.0	7.7	97.0		.250	2177.8
	5.00	87.41	.375	1.840	71.0	58.0	8.0	96.0		.250	2175.9
	5.00	91.00	.260	1.840	73.0	60.0	8.0	95.0		.250	1810.2
	5.00	94.54	.290	1.840	73.0	60.0	8.0	95.0		.250	1911.7
	5.00	98.09	.325	1.840	73.0	61.0	8.0	94.0		.250	2022.0
	5.00	101.70	.405	1.840	74.0	62.0	8.0	94.0		.250	2257.2
	5.00	105.27	.420	1.840	74.0	62.0	8.0	95.0		.250	2300.7
	5.00	108.86	.480	1.840	76.0	63.0	9.0	94.0		.250	2457.3
	5.00	112.49	.520	1.840	76.0	64.0	9.0	94.0		.250	2557.6

APPENDIX C

OPERATIONS RESULTS

The production rates of the ARCO Chemical Company Diammonium Phosphate Plant at Fort Madison, Iowa, during the week we tested, are contained in Table C-I. During the first testing day, the process operated at 100-110% of design rate which is considered normal for this plant.

TABLE C-I

PRODUCTION RATE

<u>Date</u>	<u>Run No.</u>	<u>Tons P₂O₅/Hr</u>
21 March 1973	1	14.0
21 March 1973	2	15.3
22 March 1973	3	18.2
22 March 1973	4	16.2
22 March 1973	5	14.6

APPENDIX D

FIELD DATA

This section presents the actual field data from the testing.

MIDWEST RESEARCH INSTITUTE

RUN 1F

MRI Project Number 3585-C 23
 Field Dates 3-19--3-24-73
 Plant ARCO CHEMICAL
 Sampling Location DAP N. (GRANULATION)
 Sampling Date 3-21-73

FIELD CREW

Crew Chief	1	<u>Shea</u>
Testing Engineer	1	<u>Maxwell</u>
	2	<u>Fluppm</u>
	3	
Engr. Technician	1	<u>Bechtold</u>
	2	<u>Maloney</u>
	3	
Lab Technician	1	<u>Cunningham</u>
	2	
	3	
Process Engineer	1	<u>WEE Beck</u>
	2	
Other	1	<u>WINTON KELLY - PROJ. ENGR</u>
	2	

TRAVERSE POINT LOCATION FOR CIRCULAR DUCTS

PLANT ARCO
DATE 3/21-3/23/73
SAMPLING LOCATION DAP PLANT N. STACK
INSIDE OF FAR WALL TO
OUTSIDE OF NIPPLE, (DISTANCE A) 10' 10 1/2"
INSIDE OF NEAR WALL TO
OUTSIDE OF NIPPLE, (DISTANCE B) 10 1/2"
STACK I.D., (DISTANCE A - DISTANCE B) 10'
NEAREST UPSTREAM DISTURBANCE 85'
NEAREST DOWNSTREAM DISTURBANCE 30'
CALCULATOR Shea

10. A. $\frac{\pi(s)^2}{+++}$

SCHEMATIC OF SAMPLING LOCATION

[illegible]

F-1A

SCHEMATIC OF TRAVERSE POINT LAYOUT

TRAVERSE POINT NUMBER	VELOCITY HEAD (Δp_s) , in.H ₂ O	STACK TEMPERATURE (T_s) , °F
AVERAGE		

NOMOGRAPH DATA

PLANT ARCO
 DATE 21 March 73
 SAMPLING LOCATION DAP North stack

CALIBRATED PRESSURE DIFFERENTIAL ACROSS ORIFICE, in. H ₂ O	ΔH_0	
AVERAGE METER TEMPERATURE (AMBIENT + 20 °F), °F	$T_{m \text{ avg.}}$	68
PERCENT MOISTURE IN GAS STREAM BY VOLUME	B_{wo}	20% assume
BAROMETRIC PRESSURE AT METER, in. Hg	P_m	29.8
STATIC PRESSURE IN STACK, in. Hg $+0.35'' \text{ H}_2\text{O}$ ($P_m \pm 0.073 \times \text{STACK GAUGE PRESSURE in in. H}_2\text{O}$)	P_s	29.813 29.8
RATIO OF STATIC PRESSURE TO METER PRESSURE	P_s/P_m	1.0
AVERAGE STACK TEMPERATURE, °F	$T_{s \text{ avg.}}$	102
AVERAGE VELOCITY HEAD, in. H ₂ O	$\Delta p_{\text{avg.}}$	0.4
MAXIMUM VELOCITY HEAD, in. H ₂ O	$\Delta p_{\text{max.}}$	0.44
C FACTOR		0.72
CALCULATED NOZZLE DIAMETER, in.		.25
ACTUAL NOZZLE DIAMETER, in.		.25
REFERENCE Δp , in. H ₂ O		.65 102

RUN F-1

DRY MOLECULAR WEIGHT DETERMINATION

PLANT ARCO COMMENTS: _____
 DATE 2 March 73
 SAMPLING TIME (24-hr CLOCK) 1150 - 1200
 SAMPLING LOCATION DAP North Stack Port #3 Point 1 1/2
 SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS) INT
 ANALYTICAL METHOD ORSAT
 AMBIENT TEMPERATURE 45 °F
 OPERATOR FLIPPIN

RUN GAS	1		2		3		AVERAGE NET VOLUME	MULTIPLIER	MOLECULAR WEIGHT OF STACK GAS (DRY BASIS) M _d , lb/lb-mole
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET			
CO ₂	.4	.4	20.2	.2	.2	.2	2.66	44/100	
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)	20.8	20.4	20.7	20.5	20.9	20.7	20.54	32/100	
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)	20.8	0	20.7	0	20.9	0	0	28/100	
N ₂ (NET IS 100 MINUS ACTUAL CO READING)								28/100	
TOTAL									

FIELD DATA

PLANT ARCO
 DATE 2/21/73
 SAMPLING LOCATION 2AD
 SAMPLE TYPE FLOURIDE
 RUN NUMBER F-1
 OPERATOR SLOW
 AMBIENT TEMPERATURE 43
 BAROMETRIC PRESSURE 29.8
 STATIC PRESSURE, (P_s) 4.29 +
 FILTER NUMBER (S) 1 F

PROBE LENGTH AND TYPE 3' 61
 NOZZLE I.D. 2.5
 ASSUMED MOISTURE, % 20
 SAMPLE BOX NUMBER 8
 METER BOX NUMBER 4
 METER ΔH 1.8
 C FACTOR 72
 PROBE HEATER SETTING 50
 HEATER BOX SETTING —
 REFERENCE Δp 6.5 - 10.2

yellow Pitot
 Red Orifice

SCHEMATIC OF TRAVERSE POINT LAYOUT
 READ AND RECORD ALL DATA EVERY 5 MINUTES

TRAVERSE POINT NUMBER	SAMPLING TIME, min	CLOCK TIME (24-hr CLOCK)	GAS METER READING (V _m), ft ³	VELOCITY HEAD (ΔP_s), in. H ₂ O	ORIFICE PRESSURE DIFFERENTIAL (ΔH), in. H ₂ O		STACK TEMPERATURE (T _s), °F	DRY GAS METER TEMPERATURE		PUMP VACUUM, in. Hg	SAMPLE BOX TEMPERATURE, °F	IMPINGER TEMPERATURE, °F
					DESIRED	ACTUAL		INLET (T _{m in}), °F	OUTLET (T _{m out}), °F			
	5		503.12				110					
1/1	0	1049	7.5	0.24	0.66	0.66	106	46	41			
1	5	1057	75.00	0.24	0.66	0.66	105	50	47	5		170
2	10	1102	97.70	0.24	0.66	0.66	105	54	50	3		
2	5	1107	115.40	0.2	0.57	0.57	105	55	50	3		
	10	1112*	131.57	0.2	0.57	0.57	107	57	53	5		200
3	5	1120	15.820	0.3	.85	.85	106	59	54	5		
	10	1125	18.415	0.3	0.85	.85	107	61	55	5	75	180
2/1	5	1149	20.810	0.26	0.74	0.74	107	55	55	5		180
	10	1154*	23.260	0.26	0.74	0.74	107	62	56	5		
2	5	1200	25.690	0.4	0.74	0.74	108	65	57	5		200
	10	1205	28.140	0.26	0.74	0.74	108	68	58	5		200
3	5	1230	29.562	0.07	0.21	0.21	108	56	58	3		
	10	1235	30.854	0.07	0.21	0.21	109	58	59	3	30.854-V	
3/1	5	1250	33.550	0.39	1.1	1.1	109	60	57	10		170
	10	1255	36.360	0.39	1.1	1.1	115	63	59	6.5		175
2	5	1300	39.33	0.45	1.28	1.28	120	67	58	7.5		185
	10	1305	42.42	0.46	1.3	1.3	120	69	59	7.0	65	182
3	5	1310	45.550	0.45	1.28	1.28	118	72	60	8.0		182
	10	1315	48.810	0.49	1.39	1.39	118	74	61	8.0		188
4/1	5	1330	51.500	0.35	1.0	1.0	112	60	59	6.5	65	170
	10	1335	54.280	0.41	1.2	1.2	111	65	60	7		185
2	5	1340	57.360	0.41	1.2	1.2	112	71	60	8		190
	10	1345	60.550	0.41	1.2	1.2	112	72	62	8		

COMMENTS:

ARCO

[illegible]

ANALYTICAL DATA

PLANT ARCO
 DATE 3-21-73
 SAMPLING LOCATION DAP (Granulation) N
 SAMPLE TYPE Fluoride
 RUN NUMBER (1-FLORIDE) F-1
 SAMPLE BOX NUMBER 3
 CLEAN-UP MAN CUNNINGHAM

COMMENTS:

FRONT HALF

LABORATORY RESULTS

ACETONE WASH OF NOZZLE, PROBE, CYCLONE (BYPASS),
 FLASK, FRONT HALF OF FILTER HOLDER

CONTAINER _____ mg

FILTER NUMBER _____

CONTAINER _____ mg

FRONT HALF SUBTOTAL _____ mg

BACK HALF

IMPINGER CONTENTS AND WATER WASH OF
 IMPINGERS, CONNECTORS, AND BACK
 HALF OF FILTER HOLDER

CONTAINER _____ mg

ETHER-CHLOROFORM
EXTRACTION _____ mg

ACETONE WASH OF IMPINGERS, CONNECTORS,
 AND BACK HALF OF FILTER HOLDER

CONTAINER _____ mg

BACK HALF SUBTOTAL _____ mg

TOTAL WEIGHT _____ mg

MOISTURE

IMPINGERS
 FINAL VOLUME 266 ml
 INITIAL VOLUME 200 ml
 NET VOLUME 66 ml

SILICA GEL
 FINAL WEIGHT 669.7 g
 INITIAL WEIGHT 656.6 g
 NET WEIGHT 13.1 g

EPA (Dur) 231
 4/72

Cyclone moisture 12.2 ml.
Final Vol. w/wash 401 ml
+ 20-sec. wash
421
125 ml probe wash
546 Total
 TOTAL MOISTURE 49.1 g
91.3

936,054

PROBE LENGTH AND TYPE 6
NOZZLE I.D. 1/4"
ASSUMED MOISTURE, % 20%
SAMPLE BOX NUMBER 9
METER BOX NUMBER 6
METER ΔH @ 1.84
C FACTOR 175
PROBE HEATER SETTING 50
HEATER BOX SETTING 195°F
REFERENCE ΔH 65

47

Point #3

EPA (Dut) 235

ANALYTICAL DATA

PLANT ARCO
 DATE 3/21/73
 SAMPLING LOCATION DAP N. STACK
 SAMPLE TYPE Ammonia
 RUN NUMBER NH₃-1
 SAMPLE BOX NUMBER _____
 CLEAN-UP MAN Cunningham

COMMENTS:

FRONT HALF

LABORATORY RESULTS

ACETONE WASH OF NOZZLE, PROBE, CYCLONE (BYPASS),
 FLASK, FRONT HALF OF FILTER HOLDER

CONTAINER _____ mg

FILTER NUMBER _____

CONTAINER _____ mg

FRONT HALF SUBTOTAL _____ mg

BACK HALF

IMPINGER CONTENTS AND WATER WASH OF
 IMPINGERS, CONNECTORS, AND BACK
 HALF OF FILTER HOLDER

CONTAINER _____ mg

ETHER-CHLOROFORM
 EXTRACTION _____ mg

ACETONE WASH OF IMPINGERS, CONNECTORS,
 AND BACK HALF OF FILTER HOLDER

CONTAINER _____ mg

BACK HALF SUBTOTAL _____ mg

TOTAL WEIGHT _____ mg

$H_2SO_4 (30g/L)$

MOISTURE

IMPINGERS

FINAL VOLUME 260 ml

INITIAL VOLUME 200 ml

NET VOLUME 60 ml

SILICA GEL

FINAL WEIGHT 636.3 g

INITIAL WEIGHT 625.8 g

NET WEIGHT 10.5 g

TOTAL MOISTURE 70.5 g

EPA (Dur) 231

4/72

NOMOGRAPH DATA

PLANT ARCO
 DATE 3/21/73
 SAMPLING LOCATION DAP N. STACK

CALIBRATED PRESSURE DIFFERENTIAL ACROSS ORIFICE, in. H ₂ O	ΔH_0	1.8
AVERAGE METER TEMPERATURE (AMBIENT + 20 °F), °F	$T_{m \text{ avg.}}$	70
PERCENT MOISTURE IN GAS STREAM BY VOLUME	B_{wo}	7%
BAROMETRIC PRESSURE AT METER, in. Hg	P_m	29.78
STATIC PRESSURE IN STACK, in. Hg ($P_m \pm 0.073 \times \text{STACK GAUGE PRESSURE in in. H}_2\text{O}$)	P_s	29.73
RATIO OF STATIC PRESSURE TO METER PRESSURE	P_s/P_m	1
AVERAGE STACK TEMPERATURE, °F	$T_{s \text{ avg.}}$	111
AVERAGE VELOCITY HEAD, in. H ₂ O	$\Delta p_{\text{avg.}}$	1.37
MAXIMUM VELOCITY HEAD, in. H ₂ O	$\Delta p_{\text{max.}}$	1.48
C FACTOR		0.94
CALCULATED NOZZLE DIAMETER, in.		0.25
ACTUAL NOZZLE DIAMETER, in.		0.25
REFERENCE Δp , in. H ₂ O		0.52

Run F-2

DRY MOLECULAR WEIGHT DETERMINATION

PLANT ARCO COMMENTS: _____
 DATE 3/21/73
 SAMPLING TIME (24-hr CLOCK) 1620 - 1650
 SAMPLING LOCATION DAP #3 Port Point 1 1/2
 SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS) INT
 ANALYTICAL METHOD ORSAT
 AMBIENT TEMPERATURE 50
 OPERATOR FLIPPIN

RUN GAS	1		2		3		AVERAGE NET VOLUME	MULTIPLIER	MOLECULAR WEIGHT OF STACK GAS (DRY BASIS) M _d , lb/lb-mole
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET			
CO ₂		16		17		16		44/100	
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)	21.8	21.2	21.6	20.9	21.4	20.8		32/100	
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)	21.8	0	21.6	0	21.4	0		28/100	
N ₂ (NET IS 100 MINUS ACTUAL CO READING)								28/100	
TOTAL									

F1.-2

FIELD DATA

PLANT ARCO
 DATE 3/21/73
 SAMPLING LOCATION DAP N. STATION
 SAMPLE TYPE FL
 RUN NUMBER 2
 OPERATOR Shu
 AMBIENT TEMPERATURE 50
 BAROMETRIC PRESSURE 29.78
 STATIC PRESSURE, (P_s) 0.35
 FILTER NUMBER (s) 2

PROBE LENGTH AND TYPE 3'61
 NOZZLE I.D. 1/4"
 ASSUMED MOISTURE, % 20.50
 SAMPLE BOX NUMBER 6
 METER BOX NUMBER 4
 METER ΔH 1.50
 C FACTOR .72 * .94
 PROBE HEATER SETTING 50
 HEATER BOX SETTING 52
 REFERENCE Δp 52

52 to Ref

LOCK ON

SCHEMATIC OF TRAVERSE POINT LAYOUT

READ AND RECORD ALL DATA EVERY 5 MINUTES

TRAVERSE POINT NUMBER	SAMPLING TIME, min	CLOCK TIME (24-hr CLOCK)	GAS METER READING (V _m), ft ³	VELOCITY HEAD (ΔP _s), in. H ₂ O	ORIFICE PRESSURE DIFFERENTIAL (ΔH), in. H ₂ O		STACK TEMPERATURE (T _s), °F	DRY GAS METER TEMPERATURE		PUMP VACUUM, in. Hg	SAMPLE BOX TEMPERATURE, °F	IMPINGER TEMPERATURE, °F
					DESIRED	ACTUAL		INLET (T _{m in}), °F	OUTLET (T _{m out}), °F			
1/1	5	1609	66.881	0.35	102	102	110	54	53	4		
	10	1614	72.46	0.35	102	102	110	59	54	4		50
2	5	1619	75.34	0.38	112	112	109	67	55	4		
	10	1624	78.56	0.40	122	122	109	72	57	4	82	
3	5	1629	81.30	0.33	110	100	120	75	59	4		50
	10	1634	84.122	0.33	100	100	120	76	61	4		
2/1	5	1650	86.85	0.28	89	89	125	67	62	4		
	10	1655	89.75	0.32	106	106	125	70	63	4	95	
2	5	1700	92.460	0.27	95	95	125	76	64	4		
	10	1705	95.240	0.27	95	95	125	78	64	4		
3	5	1710	97.300	0.09	32	32	122	76	66	2		
	10	1715	98.991	0.09	32	32	122	74	66	2		
3/1	5	1728	102.28	0.405	145	145	120	65	65	5	69	
	10	1733	105.700	0.405	145	145	110	70	64	5.5		
2	5	1738	108.200	0.46	160	160	109	76	64	6.0		
	10	1743	112.800	0.46	160	160	109	80	65	6.0	61	
3	5	1748	116.340	0.48	170	170	109	80	66	6.0		50
	10	1753	119.924	0.48	170	170	108	81	66	6.0		
4/1	5	1800	123.150	0.35	125	125	109	67	64	5.0		
	10	1805	126.360	0.35	125	125	105	70	63	5.0		
4/2	5	1815	129.740	0.41	145	145	101	71	63	5.5	55	
	10	1820	133.120	0.41	145	145	100	72	63	6.0		

COMMENTS:

H/min

F/2

ANALYTICAL DATA

PLANT ARCO
 DATE 3-21-73
 SAMPLING LOCATION DAP (GRANULATION) N
 SAMPLE TYPE Fluoride
 RUN NUMBER F-2
 SAMPLE BOX NUMBER _____
 CLEAN-UP MAN CUNNINGHAM

COMMENTS:

FRONT HALF

LABORATORY RESULTS

ACETONE WASH OF NOZZLE, PROBE, CYCLONE (BYPASS),
 FLASK, FRONT HALF OF FILTER HOLDER

CONTAINER _____ mg

FILTER NUMBER _____

CONTAINER _____ mg

FRONT HALF SUBTOTAL _____ mg

BACK HALF

IMPINGER CONTENTS AND WATER WASH OF
 IMPINGERS, CONNECTORS, AND BACK
 HALF OF FILTER HOLDER

CONTAINER _____ mg

ETHER-CHLOROFORM
 EXTRACTION _____ mg

ACETONE WASH OF IMPINGERS, CONNECTORS,
 AND BACK HALF OF FILTER HOLDER

CONTAINER _____ mg

BACK HALF SUBTOTAL _____ mg

TOTAL WEIGHT _____ mg

H₂O

MOISTURE

IMPINGERS
 FINAL VOLUME 276 ml 288
 INITIAL VOLUME 200 ml 200
 NET VOLUME 76 ml 88

SILICA GEL
 FINAL WEIGHT 632.9 g _____ g
 INITIAL WEIGHT 618.2 g _____ g
 NET WEIGHT 14.7 g _____ g

EPA (Dur) 231
 4/72

7.2 ml - cyclone
 Imp. water = 288 ml.
 After wash 2 450 ml.
 PROBE WASH - 4214 ml
 GRAD WASH - 664 ml
 + 10 ml
 TOTAL MOISTURE 674 ml

Total moisture 102.7
 + cyclone 7.2
 109.9

$$\underline{\text{NH}_3}$$

PROBE LENGTH AND TYPE 6' 6 l.
NOZZLE I.D. 1/4"
ASSUMED MOISTURE, % 20%
SAMPLE BOX NUMBER 9
METER BOX NUMBER 6
METER ΔH @ 1.84
C FACTOR 5.72
PROBE HEATER SETTING ~~250~~ 6
HEATER BOX SETTING 250
REFERENCE ΔH _____

READ AND RECORD ALL DATA EVERY _____ MINUTES

[illegible]

COMMENTS:

Port # 4

54

ANALYTICAL DATA

PLANT ARCO
 DATE 3-21-73
 SAMPLING LOCATION DAP (GRANULATION)
 SAMPLE TYPE Ammonia
 RUN NUMBER NH₃ - 2
 SAMPLE BOX NUMBER 9
 CLEAN-UP MAN CUNNINGHAM

COMMENTS:

FRONT HALF

LABORATORY RESULTS

ACETONE WASH OF NOZZLE, PROBE, CYCLONE (BYPASS),
 FLASK, FRONT HALF OF FILTER HOLDER

CONTAINER _____ mg

FILTER NUMBER _____

CONTAINER _____ mg

FRONT HALF SUBTOTAL _____ mg

BACK HALF

IMPINGER CONTENTS AND WATER WASH OF
 IMPINGERS, CONNECTORS, AND BACK
 HALF OF FILTER HOLDER

CONTAINER _____ mg

ETHER-CHLOROFORM
 EXTRACTION _____ mg

ACETONE WASH OF IMPINGERS, CONNECTORS,
 AND BACK HALF OF FILTER HOLDER

CONTAINER _____ mg

BACK HALF SUBTOTAL _____ mg

TOTAL WEIGHT _____ mg

MOISTURE

IMPINGERS
 FINAL VOLUME 256 ml
 INITIAL VOLUME 200 ml
 NET VOLUME 56 ml

SILICA GEL
 FINAL WEIGHT 646.0 g
 INITIAL WEIGHT 636.3 g
 NET WEIGHT 9.7 g

EPA (Dur) 231
 4/72

H₂SO₄ (30g/l)

Vol after washing 321
 +20
 341
 +41
 Total = 382

TOTAL MOISTURE 65.7 g

NOMOGRAPH DATA

PLANT ARCO
 DATE 22 March 73
 SAMPLING LOCATION DAP North stack

CALIBRATED PRESSURE DIFFERENTIAL ACROSS ORIFICE, in. H ₂ O	ΔH_0	1.80
AVERAGE METER TEMPERATURE (AMBIENT + 20 °F), °F	$T_{m\text{ avg.}}$	68 74.2
PERCENT MOISTURE IN GAS STREAM BY VOLUME	B_{wo}	7%
BAROMETRIC PRESSURE AT METER, in. Hg	P_m	28.72
STATIC PRESSURE IN STACK, in. Hg ($P_m \pm 0.073 \times \text{STACK GAUGE PRESSURE in in. H}_2\text{O}$)	P_s	29.733 0.13 + 20 0.35
RATIO OF STATIC PRESSURE TO METER PRESSURE	P_s/P_m	1
AVERAGE STACK TEMPERATURE, °F	$T_{s\text{ avg.}}$	110
AVERAGE VELOCITY HEAD, in. H ₂ O	$\Delta p_{\text{ avg.}}$	0.40
MAXIMUM VELOCITY HEAD, in. H ₂ O	$\Delta p_{\text{ max.}}$	0.48
C FACTOR		0.94
CALCULATED NOZZLE DIAMETER, in.		.25
ACTUAL NOZZLE DIAMETER, in.		.25
REFERENCE Δp , in. H ₂ O		.52

FL-3

0.0001 1.70 min

FIELD DATA

PLANT ARCO
 DATE 3/22/73
 SAMPLING LOCATION DAP N. STACK
 SAMPLE TYPE FL
 RUN NUMBER 3
 OPERATOR Shen
 AMBIENT TEMPERATURE 65°F
 BAROMETRIC PRESSURE 29.72
 STATIC PRESSURE, (P_s) +0.35
 FILTER NUMBER (s) 3

PROBE LENGTH AND TYPE 3'61
 NOZZLE I.D. 1/4
 ASSUMED MOISTURE, % 7.0
 SAMPLE BOX NUMBER 4
 METER BOX NUMBER 4
 METER ΔH 4.80
 C FACTOR 54
 PROBE HEATER SETTING 50-60
 HEATER BOX SETTING 50-60
 REFERENCE Δp 52

SCHEMATIC OF TRAVERSE POINT LAYOUT

READ AND RECORD ALL DATA EVERY 5 MINUTES

TRAVERSE POINT NUMBER		CLOCK TIME (24-hr CLOCK)	GAS METER READING (V _m), ft ³	VELOCITY HEAD (Δp _s), in. H ₂ O	ORIFICE PRESSURE DIFFERENTIAL (ΔH), in. H ₂ O		STACK TEMPERATURE (T _s), °F	DRY GAS METER TEMPERATURE		PUMP VACUUM, in. Hg	SAMPLE BOX TEMPERATURE, °F	IMPINGER TEMPERATURE, °F	Probe Temp
					DESIRED	ACTUAL		INLET (T _{m in}), °F	OUTLET (T _{m out}), °F				
		<u>1004</u>	<u>140.117</u>	<u>0.23</u>	<u>0.55</u>	<u>0.73</u>							
P1/1	5	<u>1009</u>	<u>142.980</u>	<u>0.15</u>	<u>0.55</u>	<u>0.73</u>	<u>109</u>	<u>48</u>	<u>48</u>	<u>5</u>	<u>60</u>	<u>245</u>	
	10	<u>1014</u>	<u>145.400</u>	<u>0.23</u>	<u>0.75</u>	<u>0.75</u>	<u>110</u>	<u>54</u>	<u>50</u>	<u>5</u>	<u>65</u>	<u>185</u>	
2	5	<u>1019</u>	<u>148.200</u>	<u>0.29</u>	<u>1.02</u>	<u>1.02</u>	<u>110</u>	<u>55</u>	<u>50</u>	<u>6</u>			
	10	<u>1024</u>	<u>151.085</u>	<u>0.31</u>	<u>1.11</u>	<u>1.11</u>	<u>108</u>	<u>54</u>	<u>51</u>	<u>7</u>			
3	5	<u>1024</u>	<u>153.780</u>	<u>0.25</u>	<u>.91</u>	<u>.91</u>	<u>109</u>	<u>58</u>	<u>52</u>	<u>6</u>			
	10	<u>1034</u>	<u>156.476</u>	<u>0.26</u>	<u>.92</u>	<u>.92</u>	<u>108</u>	<u>60</u>	<u>52</u>	<u>6</u>	<u>61</u>		<u>162</u>
P2-1	5	<u>1044</u>	<u>159.036</u>	<u>0.24</u>	<u>.87</u>	<u>.87</u>	<u>106</u>	<u>50</u>	<u>52</u>	<u>5</u>	<u>55</u>		<u>114</u>
	10	<u>1054</u>	<u>161.576</u>	<u>0.23</u>	<u>0.80</u>	<u>0.80</u>	<u>106</u>	<u>56</u>	<u>52</u>	<u>5</u>	<u>58</u>		<u>130</u>
2	5	<u>1059</u>	<u>163.855</u>	<u>0.19</u>	<u>0.66</u>	<u>0.66</u>	<u>108</u>	<u>60</u>	<u>53</u>	<u>4</u>	<u>60</u>		<u>143</u>
	10	<u>1104</u>	<u>166.215</u>	<u>0.20</u>	<u>0.69</u>	<u>0.69</u>	<u>110</u>	<u>62</u>	<u>54</u>	<u>4</u>	<u>66</u>		<u>158</u>
3	5	<u>1109</u>	<u>167.483</u>	<u>0.03</u>	<u>0.10</u>	<u>0.10</u>	<u>114</u>	<u>61</u>	<u>55</u>	<u>2</u>	<u>67</u>		<u>132</u>
	10	<u>1114</u>	<u>168.452</u>	<u>0.03</u>	<u>0.10</u>	<u>0.10</u>	<u>113</u>	<u>60</u>	<u>56</u>	<u>2</u>	<u>69</u>	<u><50</u>	<u>132</u>
P3-1	5	<u>1124</u>	<u>171.792</u>	<u>0.36</u>	<u>1.35</u>	<u>1.35</u>	<u>115</u>	<u>57</u>	<u>56</u>	<u>8</u>	<u>67</u>		<u>125</u>
	10	<u>1134</u>	<u>174.935</u>	<u>0.36</u>	<u>1.35</u>	<u>1.35</u>	<u>116</u>	<u>65</u>	<u>57</u>	<u>8</u>	<u>73</u>	<u>50</u>	<u>135</u>
2	5	<u>1139</u>	<u>178.351</u>	<u>0.41</u>	<u>1.57</u>	<u>1.57</u>	<u>116</u>	<u>71</u>	<u>59</u>	<u>8</u>	<u>75</u>		<u>144</u>
	10	<u>1144</u>	<u>181.815</u>	<u>0.41</u>	<u>1.57</u>	<u>1.57</u>	<u>115</u>	<u>74</u>	<u>60</u>	<u>8.5</u>	<u>72</u>		<u>157</u>
3	5	<u>1149</u>	<u>185.310</u>	<u>0.45</u>	<u>1.70</u>	<u>1.70</u>	<u>117</u>	<u>77</u>	<u>62</u>	<u>10.0</u>	<u>75</u>		<u>166</u>
	10	<u>1154</u>	<u>188.967</u>	<u>0.45</u>	<u>1.70</u>	<u>1.70</u>	<u>115</u>	<u>79</u>	<u>62</u>	<u>10</u>	<u>75</u>		<u>170</u>
P4-1	5	<u>1213</u>	<u>192.200</u>	<u>0.34</u>	<u>1.25</u>	<u>1.25</u>	<u>125</u>	<u>60</u>	<u>62</u>	<u>8.5</u>	<u>70</u>	<u>50</u>	<u>181</u>
	10	<u>1223</u>	<u>195.450</u>	<u>0.34</u>	<u>1.25</u>	<u>1.25</u>	<u>120</u>	<u>68</u>	<u>62</u>	<u>9.0</u>	<u>70</u>		<u>202</u>
2	5	<u>1228</u>	<u>198.800</u>	<u>0.39</u>	<u>1.45</u>	<u>1.45</u>	<u>118</u>	<u>70</u>	<u>62</u>	<u>9.0</u>	<u>72</u>		<u>210</u>
	10	<u>1233</u>	<u>202.170</u>	<u>0.40</u>	<u>1.50</u>	<u>1.50</u>	<u>119</u>	<u>72</u>	<u>62</u>	<u>9.0</u>	<u>74</u>		
				<u>0.40</u>									

COMMENTS:

DRY MOLECULAR WEIGHT DETERMINATION

PLANT ARCO COMMENTS: _____
 DATE 3/22/73
 SAMPLING TIME (24-hr CLOCK) 1108 - 1138
 SAMPLING LOCATION DAP N. ST Acid Port #1 Point 1 1/2
 SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS) Int
 ANALYTICAL METHOD ORSAT
 AMBIENT TEMPERATURE 46
 OPERATOR Bechtold

RUN GAS	1		2		3		AVERAGE NET VOLUME	MULTIPLIER	MOLECULAR WEIGHT OF STACK GAS (DRY BASIS) M _d , lb/lb-mole
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET			
CO ₂	0.1	0.1	0.2	0.2	0.2	0.2	0.2	44/100	
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)	20.3	20.2	20.2	20.0	20.4	20.2	20.2	32/100	
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)	20.3	0	20.2	0	20.4	0	0	28/100	
N ₂ (NET IS 100 MINUS ACTUAL CO READING)								28/100	
TOTAL									

ANALYTICAL DATA

PLANT ARCO
 DATE 3-22-73
 SAMPLING LOCATION DAP (GRANULATION) N
 SAMPLE TYPE Fluoride
 RUN NUMBER F-3
 SAMPLE BOX NUMBER 3
 CLEAN-UP MAN CUNNINGHAM

COMMENTS:

FRONT HALF

LABORATORY RESULTS

ACETONE WASH OF NOZZLE, PROBE, CYCLONE (BYPASS),
 FLASK, FRONT HALF OF FILTER HOLDER

CONTAINER _____ mg

FILTER NUMBER _____

CONTAINER _____ mg

FRONT HALF SUBTOTAL _____ mg

BACK HALF

IMPINGER CONTENTS AND WATER WASH OF
 IMPINGERS, CONNECTORS, AND BACK
 HALF OF FILTER HOLDER

CONTAINER _____ mg

ETHER-CHLOROFORM
EXTRACTION _____ mg

ACETONE WASH OF IMPINGERS, CONNECTORS,
 AND BACK HALF OF FILTER HOLDER

CONTAINER _____ mg

BACK HALF SUBTOTAL _____ mg

TOTAL WEIGHT _____ mg

MOISTURE

IMPINGERS
 FINAL VOLUME 274 ml
 INITIAL VOLUME 200 ml
 NET VOLUME 74 ml

SILICA GEL
 FINAL WEIGHT 684.0 g
 INITIAL WEIGHT 669.7 g
 NET WEIGHT 14.3 g

Glycone $\frac{9.3}{+4.0}$
 $\frac{14.1 \text{ ml.}}$
 Imp Vol = 274 ml.
 After Wash Vol = 342 ml.
 + Probe Wash + 355
 Total = 697 ml

88.3
 14.1
 TOTAL MOISTURE 102.4 g

FIELD DATA

PLANT ARCO
 DATE 3/22/73
 SAMPLING LOCATION DAF STACK
 SAMPLE TYPE NH₃
 RUN NUMBER 3
 OPERATOR Shea
 AMBIENT TEMPERATURE 45
 BAROMETRIC PRESSURE 30.35
 STATIC PRESSURE, (P_s) 3
 FILTER NUMBER (s) 3

PROBE LENGTH AND TYPE 6' 61.
 NOZZLE I.D. 1/4 790
 ASSUMED MOISTURE, % 9
 SAMPLE BOX NUMBER 6
 METER BOX NUMBER 1.84
 METER ΔH 250
 C FACTOR 7
 PROBE HEATER SETTING 250
 HEATER BOX SETTING 250
 REFERENCE Δp

SCHEMATIC OF TRAVERSE POINT LAYOUT
 READ AND RECORD ALL DATA EVERY 5 MINUTES

TRAVERSE POINT NUMBER	CLOCK TIME (24-hr CLOCK)	GAS METER READING (V _m), ft ³	VELOCITY HEAD (Δp _s), in. H ₂ O	ORIFICE PRESSURE DIFFERENTIAL (ΔH), in. H ₂ O		STACK TEMPERATURE (T _s), °F	DRY GAS METER TEMPERATURE		PUMP VACUUM, in. Hg	SAMPLE BOX TEMPERATURE, °F	HMPINGER TEMPERATURE, °F
				DESIRED	ACTUAL		INLET (T _{m in}), °F	OUTLET (T _{m out}), °F			
5	1101	24.437									
Port #3	0 TIME	24.797	0.42	1.84	1.84	10.5					
1	5 1106	28.550	0.43	1.84	1.84	97	50	45	8	164	142
2	10 1111	32.190	0.43	1.84	1.84	97	60	48	8	132	162
3	15 1116	35.850	0.43	1.84	1.84	97	66	50	89	110	168
4	20 1121	39.580	0.43	1.84	1.84	98	69	52	9	122	168
5	25 1126	43.250	0.43	1.84	1.84	95	72	53	9		
6	30 1131	47.100	0.43	1.84	1.84	95	73	55	9	130	50 172
7	35 1136	50.800	0.43	1.84	1.84	95	75	56	9	130	171
8	40 1141	54.570	0.43	1.84	1.84	95	76	57	9	130	168
9	45 1146	58.320	0.44	1.84	1.84	100	76	58	9		
10	50 1151	62.090	0.44	1.84	1.84	101	76	58	9 1/2	115	170
11	55 1156	65.870	0.44	1.84	1.84	99	78	60	10	155	180
12	60 1201	69.732	0.45	1.84	1.84	98	78	60	10 1/2	120	185

COMMENTS:

NH₃-3

ANALYTICAL DATA

PLANT ARCO COMMENTS:
 DATE 3-22-73
 SAMPLING LOCATION DAP N (GRANULATION)
 SAMPLE TYPE Ammonia
 RUN NUMBER NH₃-3
 SAMPLE BOX NUMBER _____
 CLEAN-UP MAN CUNNINGHAM

FRONT HALF

LABORATORY RESULTS

ACETONE WASH OF NOZZLE, PROBE, CYCLONE (BYPASS),
 FLASK, FRONT HALF OF FILTER HOLDER

CONTAINER _____ mg

FILTER NUMBER _____

CONTAINER _____ mg

FRONT HALF SUBTOTAL _____ mg

BACK HALF

IMPINGER CONTENTS AND WATER WASH OF
 IMPINGERS, CONNECTORS, AND BACK
 HALF OF FILTER HOLDER

CONTAINER _____ mg

ETHER-CHLOROFORM
 EXTRACTION _____ mg

ACETONE WASH OF IMPINGERS, CONNECTORS,
 AND BACK HALF OF FILTER HOLDER

CONTAINER _____ mg

BACK HALF SUBTOTAL _____ mg

TOTAL WEIGHT _____ mg

MOISTURE

IMPINGERS
 FINAL VOLUME 256 ml
 INITIAL VOLUME 200 ml
 NET VOLUME 56 ml
 H₂SO₄ (30g/l)

256
 + 406 wash
 Total 662 ml

SILICA GEL
 FINAL WEIGHT 637.4 g
 INITIAL WEIGHT 627.6 g
 NET WEIGHT 9.8 g

TOTAL MOISTURE 65.8 g

F-4

NOMOGRAPH DATA

PLANT ARCO
 DATE 22 March 73
 SAMPLING LOCATION DAP- North Stack

CALIBRATED PRESSURE DIFFERENTIAL ACROSS ORIFICE, in. H ₂ O	$\Delta H_{@}$	1.80
AVERAGE METER TEMPERATURE (AMBIENT + 20 °F), °F	$T_{m\text{ avg.}}$	174
PERCENT MOISTURE IN GAS STREAM BY VOLUME	B_{wo}	7%
BAROMETRIC PRESSURE AT METER, in. Hg	P_m	29.6
STATIC PRESSURE IN STACK, in. Hg ($P_m \pm 0.073 \times \text{STACK GAUGE PRESSURE in in. H}_2\text{O}$)	P_s	99.613
RATIO OF STATIC PRESSURE TO METER PRESSURE	P_s/P_m	1
AVERAGE STACK TEMPERATURE, °F	$T_{s\text{ avg.}}$	105
AVERAGE VELOCITY HEAD, in. H ₂ O	$\Delta p_{\text{ avg.}}$	0.37
MAXIMUM VELOCITY HEAD, in. H ₂ O	$\Delta p_{\text{ max.}}$	.42
C FACTOR		.94
CALCULATED NOZZLE DIAMETER, in.		.25
ACTUAL NOZZLE DIAMETER, in.		.25
REFERENCE Δp , in. H ₂ O		0.52

FIELD DATA

PLANT ARCO
 DATE 3/22/73
 SAMPLING LOCATION DAP N. STACH
 SAMPLE TYPE FI
 RUN NUMBER 4
 OPERATOR Shea
 AMBIENT TEMPERATURE 54.0°F
 BAROMETRIC PRESSURE 29.6
 STATIC PRESSURE, (P_s) -3.5
 FILTER NUMBER (s) 4

26 cfm 0.001/min
 PROBE LENGTH AND TYPE 3' GI
 NOZZLE I.D. 1/4"
 ASSUMED MOISTURE, % 7.4
 SAMPLE BOX NUMBER
 METER BOX NUMBER 4
 METER ΔH 1.80
 C FACTOR 7.2
 PROBE HEATER SETTING .55
 HEATER BOX SETTING
 REFERENCE Δp .52

SCHEMATIC OF TRAVERSE POINT LAYOUT
 READ AND RECORD ALL DATA EVERY 5 MINUTES

TRAVERSE POINT NUMBER	CLOCK TIME (24-hr CLOCK)	GAS METER READING (V _m), ft ³	VELOCITY HEAD (ΔP _s), in. H ₂ O	ORIFICE PRESSURE DIFFERENTIAL (ΔH), in. H ₂ O		STACK TEMPERATURE (T _s), °F	DRY GAS METER TEMPERATURE		PUMP VACUUM, in. Hg	SAMPLE BOX TEMPERATURE, °F	IMPINGER TEMPERATURE, °F
				DESIRED	ACTUAL		INLET (T _{m in}), °F	OUTLET (T _{m out}), °F			
	<u>3 15:20</u>	<u>209.086</u>									
P1/1	5 15:25	211.820	0.25	0.93	0.93	105	54	54	5		160
2	10 15:30	214.640	0.27	1.00	1.00	103	59	59	5	65	
2	5 15:35	217.920	0.36	1.31	1.31	105	66	56	5	65	
	10 15:40	221.240	0.36	1.31	1.31	105	68	57	5		170
3	5 15:45	224.390	0.33	1.21	1.21	106	68	58	5	65	176
	10 15:50	227.505	0.31	1.18	1.18	106	66	58	5	65	182
P2/1	5 16:03	230.580	0.30	1.12	1.12	108	58	58	4.5	69	160
	10 16:08	233.680	0.30	1.12	1.12	116	64	58	4.5	80	191
2	5 16:13	236.235	0.22	.79	.74	117	67	60	3.5	88	204
	10 16:18	238.725	.21	.75	.75	117	67	60	3.5	85	206
3	5 16:23	240.225	.06	.22	.22	117	64	61	1.0	79	208
	10 16:28	241.490	.05	.185	.185	110	62	61	1.0	79	210
P/3	5 16:43	244.620	.36	1.29	1.29	110	56	58	3.0	66	187
	10 16:48	247.710	.36	1.29	1.29	107	61	59	5.0	67	200
2	5 16:53	250.130	.42	1.50	1.50	106	66	59	5.5	66	204
	10 16:58	254.530	.42	1.50	1.50	106	68	60	5.5	64	204
3	5 17:03	258.010	.45	1.60	1.60	103	69	60	4.0	63	204
	10 17:08	261.540	.46	1.63	1.63	103	69	60	4.0	63	208
P/4	5 17:21	264.755	.36	1.30	1.30	105	60	59	5.0	56	176
	10 17:26	267.465	.38	1.35	1.35	103	64	60	5.0	57	186
2	5 17:31	271.315	.42	1.50	1.50	107	66	60	5.5	56	187
	10 17:36	274.710	.42	1.50	1.50	107	69	60	5.5	56	188

COMMENTS:

—

190
192

F-4

RUN F-4
DRY MOLECULAR WEIGHT DETERMINATION

PLANT ARCO COMMENTS:
 DATE 3/22/73
 SAMPLING TIME (24-hr CLOCK) 1534 - 1604
 SAMPLING LOCATION DAP Port 4 IN. STACK
 SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS) INT
 ANALYTICAL METHOD CRSAT
 AMBIENT TEMPERATURE 54.0
 OPERATOR Shea

RUN GAS	1		2		3		AVERAGE NET VOLUME	MULTIPLIER	MOLECULAR WEIGHT OF STACK GAS (DRY BASIS) M _d , lb/lb-mole
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET			
CO ₂	0.4	.4	0.4	0.4	.4	.4	.4	44/100	
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)	21.0	20.6	21.0	20.6	21.0	20.6	20.6	32/100	
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)	21.0	0.0	21.0	0.0	21.0	20.6	0	28/100	
N ₂ (NET IS 100 MINUS ACTUAL CO READING)	100.0	79.0	100.0	79.0	100.0	79.0	79.0	28/100	
TOTAL									

ANALYTICAL DATA

PLANT ARCO
 DATE 3-22-73
 SAMPLING LOCATION DAP (GRAVULATION) N
 SAMPLE TYPE Fluoride
 RUN NUMBER F-7
 SAMPLE BOX NUMBER 3
 CLEAN-UP MAN CUNNINGHAM

COMMENTS:

FRONT HALF

LABORATORY RESULTS

ACETONE WASH OF NOZZLE, PROBE, CYCLONE (BYPASS),
 FLASK, FRONT HALF OF FILTER HOLDER

CONTAINER _____ mg

FILTER NUMBER _____

CONTAINER _____ mg

FRONT HALF SUBTOTAL _____ mg

BACK HALF

IMPINGER CONTENTS AND WATER WASH OF
 IMPINGERS, CONNECTORS, AND BACK
 HALF OF FILTER HOLDER

CONTAINER _____ mg

ETHER-CHLOROFORM
 EXTRACTION _____ mg

ACETONE WASH OF IMPINGERS, CONNECTORS,
 AND BACK HALF OF FILTER HOLDER

CONTAINER _____ mg

BACK HALF SUBTOTAL _____ mg

TOTAL WEIGHT	_____ mg
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MOISTURE

IMPINGERS
 FINAL VOLUME 261 ml
 INITIAL VOLUME 200 ml
 NET VOLUME 61 ml

SILICA GEL
 FINAL WEIGHT 631.8 g _____ g
 INITIAL WEIGHT 646.0 g _____ g
 NET WEIGHT 15.8 g _____ g

Cyclone — 9.6
 + 1.5
 11.1 ml.

Imp Water Total Vol = 261
 Imp Wash + 445
 Probe Wash 21.5
 Total 921 ml.

TOTAL MOISTURE 87.9 g

+ 61.8
 + 15.8
 + 11.1
 87.9

FIELD DATA *NH₃-4*

PLANT ARCO
DATE 3/23/73
SAMPLING LOCATION DAP N. STACK #4
SAMPLE TYPE NAF
RUN NUMBER 4
OPERATOR Shoa
AMBIENT TEMPERATURE 52
BAROMETRIC PRESSURE 29.8
STATIC PRESSURE, (P_s) 0.35
FILTER NUMBER (s) 4

PROBE LENGTH AND TYPE 6' gl.
NOZZLE I.D. 1/4"
ASSUMED MOISTURE, % 7
SAMPLE BOX NUMBER _____
METER BOX NUMBER 6
METER ΔH @ _____ 1.84
C FACTOR _____
PROBE HEATER SETTING 7
HEATER BOX SETTING 250
REFERENCE Δp _____

SCHEMATIC OF TRAVERSE POINT LAYOUT

READ AND RECORD ALL DATA EVERY 5 MINUTES

TRAVERSE POINT NUMBER	CLOCK TIME (24-hr CLOCK)	GAS METER READING (V _m), ft ³	VELOCITY - HEAD (Δp _s), in. H ₂ O	ORIFICE PRESSURE DIFFERENTIAL (ΔH), in. H ₂ O		STACK TEMPERATURE (T _s), °F	DRY GAS METER TEMPERATURE		PUMP VACUUM, in. Hg	SAMPLE BOX TEMPERATURE, °F PROBE	IMPINGER TEMPERATURE, °F
				DESIRED	ACTUAL		INLET (T _{m in}), °F	OUTLET (T _{m out}), °F			
1	8:09:37	281.647	1.9	1.84	104	53	54	4	59		
02	9:48	69.808	38/39	1.84	108	56	54	6.5	115		
13	9:53	73.24	38	1.84	100	61	54	~8.0	145		
24	58	76.88	38	1.84	100	66	55	7.75	180		
35	10:03	80.34	38	1.84	98	68	56	7.75	136		
46	08	83.86	37/38	1.84	97	70	57	7.75	192		
57	13	87.41	37/38	1.84	96	71	58	~8.0	198		
68	18	90.00	25/27	1.84	95	73	60	~8.0	200		
79	23	94.54	28/30	1.84	95	73	60	~8.0	150		
810	28	98.09	31/32	1.84	94	73	61	~8.0	103		
911	33	101.70	40/41	1.84	94	74	62	~8.0	110		
1012	38	105.27	43/45	1.84	95	74	62	~8.0	168		
11	43	108.86	48	1.84	94	76	63	9.0	198		
17	48	112.494	52	1.84	94	76	64	~9.0	200		

COMMENTS:

NH₃-4

ANALYTICAL DATA

PLANT ARCO
DATE 3-23-73
SAMPLING LOCATION DAP N (GRANULATION)
SAMPLE TYPE Ammonia
RUN NUMBER NH₃-4
SAMPLE BOX NUMBER 9
CLEAN-UP MAN CUNNINGHAM

COMMENTS:

FRONT HALF

LABORATORY RESULTS

ACETONE WASH OF NOZZLE, PROBE, CYCLONE (BYPASS),
FLASK, FRONT HALF OF FILTER HOLDER

CONTAINER _____ mg

FILTER NUMBER _____

CONTAINER _____ mg

FRONT HALF SUBTOTAL _____ mg

BACK HALF

IMPINGER CONTENTS AND WATER WASH OF
IMPINGERS, CONNECTORS, AND BACK
HALF OF FILTER HOLDER

CONTAINER _____ mg

ETHER-CHLOROFORM
EXTRACTION _____ mg

ACETONE WASH OF IMPINGERS, CONNECTORS,
AND BACK HALF OF FILTER HOLDER

CONTAINER _____ mg

BACK HALF SUBTOTAL _____ mg

TOTAL WEIGHT _____ mg

MOISTURE

IMPINGERS
FINAL VOLUME 262 ml
INITIAL VOLUME 200 ml
NET VOLUME 62 ml

H₂SO₄ (30g/l)

SILICA GEL
FINAL WEIGHT 6486 g
INITIAL WEIGHT 6374 g
NET WEIGHT 112 g

Imp. Water 262
wash + 309
571 ml
wash. + 25 ml
596 ml

TOTAL MOISTURE _____ g

NOMOGRAPH DATA

PLANT AZCO
 DATE 23 March 73
 SAMPLING LOCATION DAP North Stack

CALIBRATED PRESSURE DIFFERENTIAL ACROSS ORIFICE, in. H ₂ O	ΔH_0	1.80
AVERAGE METER TEMPERATURE (AMBIENT + 20°F), °F	$T_{m\text{avg.}}$	73
PERCENT MOISTURE IN GAS STREAM BY VOLUME	B_{w0}	7%
BAROMETRIC PRESSURE AT METER, in. Hg	P_m	29.8
STATIC PRESSURE IN STACK, in. Hg ($P_m \pm 0.073 \times \text{STACK GAUGE PRESSURE in in. H}_2\text{O}$)	P_s	29.813
RATIO OF STATIC PRESSURE TO METER PRESSURE	P_s/P_m	1.00
AVERAGE STACK TEMPERATURE, °F	$T_{s\text{avg.}}$	110
AVERAGE VELOCITY HEAD, in. H ₂ O	$\Delta p_{\text{avg.}}$	0.27
MAXIMUM VELOCITY HEAD, in. H ₂ O	$\Delta p_{\text{max.}}$	0.36
C FACTOR		0.84
CALCULATED NOZZLE DIAMETER, in.		.25"
ACTUAL NOZZLE DIAMETER, in.		.25"
REFERENCE Δp , in. H ₂ O		.52

FIELD DATA

F-5

PLANT ARCO
 DATE 3/23/73
 SAMPLING LOCATION DAP STACK
 SAMPLE TYPE FL
 RUN NUMBER 5
 OPERATOR Shod
 AMBIENT TEMPERATURE 52
 BAROMETRIC PRESSURE 29.8
 STATIC PRESSURE, (P_s) +0.39 Port 3 Point 3 @ 1131
 FILTER NUMBER (s) 5

PROBE LENGTH AND TYPE 3' 61
 NOZZLE I.D. 1/4
 ASSUMED MOISTURE, % 7%
 SAMPLE BOX NUMBER 4
 METER BOX NUMBER 4
 METER ΔH 1.80
 C FACTOR 60
 PROBE HEATER SETTING 60
 HEATER BOX SETTING 52
 REFERENCE Δp 52

SCHEMATIC OF TRAVERSE POINT LAYOUT
 READ AND RECORD ALL DATA EVERY 5 MINUTES

TRAVERSE POINT NUMBER	SAMPLING TIME, min	CLOCK TIME (24-hr CLOCK)	GAS METER READING (V _m), ft ³	VELOCITY HEAD (Δp _s), in. H ₂ O	ORIFICE PRESSURE DIFFERENTIAL (ΔH), in. H ₂ O		STACK TEMPERATURE (T _s), °F	DRY GAS METER TEMPERATURE		PUMP VACUUM, in. Hg	SAMPLE BOX TEMPERATURE, °F	IMPINGER TEMPERATURE, °F
					DESIRED	ACTUAL		INLET (T _{m in}), °F	OUTLET (T _{m out}), °F			
	5	0939	281.647									
P111	5	0944	283.94	0.19	0.685	0.685	109	53	54	4	59	
	10	0949	286.32	0.19	0.685	0.685	110	56	54	5	61	275
2	5	0954	289.03	0.26	0.93	0.93	109	60	55	5	65	190
	10	0959	291.80	0.27	0.96	0.96	109	61	56	5	61	160
3	5	1004	294.41	0.23	0.83	0.83	107	64	57	5+	65	175
	10	1009	297.029	0.22	0.78	0.78	110	64	58	5.5	65	180
P21	5	1019	297.299.500	0.21	0.75	0.75	108	58	58	4	64	50 156
	10	1029	302.000	0.21	0.75	0.75	110	61	59	5	69	180
2	5	1034	304.24	0.15	0.57	0.57	110	64	60	4	65	185
	10	1039	306.44	0.15	0.57	0.57	110	66	60	4	70	190
3	5	1044	307.73	0.01	0.11	0.11	110	63	61	2	68	199
	10	1049	308.928	0.01	0.11	0.11	110	63	62	2	70	208
P31	5	1103	311.64	0.28	1.00	1.00	112	62	62	6	70	210
	10	1108	314.48	0.28	1.00	1.00	112	68	63	6	71	212
2	5	1113	317.55	0.34	1.21	1.21	112	70	64	7	72	209
	10	1118	320.65	0.33	1.18	1.18	112	72	65	7	75	205
3	5	1123	323.71	0.36	1.30	1.30	112	76	66	8	79	212
	10	1128	326.800	0.36	1.30	1.30	110	76	67	8	75	220
P41	5	1143	329.910	0.29	1.05	1.05	110	64	65	7	70	195
	10	1148	332.88	0.29	1.05	1.05	112	68	65	7	70	200
2	5	1153	335.90	0.33	1.20	1.20	110	72	65	8	70	200
	10	1158	338.95	0.33	1.20	1.20	110	72	66	8	69	201

COMMENTS:

210
218

72

RUN F-5 DRY MOLECULAR WEIGHT DETERMINATION

PLANT ARCO COMMENTS: _____
 DATE 3/23/73
 SAMPLING TIME (24-hr CLOCK) 1005 - 1035
 SAMPLING LOCATION DAP N. STACK PORT 3 Point 1 1/2
 SAMPLE TYPE (BAG, INTEGRATED, CONTINUOUS) INT
 ANALYTICAL METHOD ORSAT
 AMBIENT TEMPERATURE 52
 OPERATOR Shea

RUN GAS	1		2		3		AVERAGE NET VOLUME	MULTIPLIER	MOLECULAR WEIGHT OF STACK GAS (DRY BASIS) M _d , lb/lb-mole
	ACTUAL READING	NET	ACTUAL READING	NET	ACTUAL READING	NET			
CO ₂	0.2	0.2	0.2	0.2	0.2	0.2	0.2	44/100	
O ₂ (NET IS ACTUAL O ₂ READING MINUS ACTUAL CO ₂ READING)	20.8	20.6	20.8	20.6	20.8	20.6	20.6	32/100	
CO (NET IS ACTUAL CO READING MINUS ACTUAL O ₂ READING)	20.8	0	20.8	0	20.8	0	0	28/100	
N ₂ (NET IS 100 MINUS ACTUAL CO READING)		79.2		79.2		79.2	79.2	28/100	
TOTAL									

ANALYTICAL DATA

PLANT ARCO

COMMENTS:

DATE 3-23-73SAMPLING LOCATION DAP N (GRANULATION)SAMPLE TYPE FluorideRUN NUMBER F-5

SAMPLE BOX NUMBER _____

CLEAN-UP MAN CUNNINGHAMFRONT HALF

LABORATORY RESULTS

ACETONE WASH OF NOZZLE, PROBE, CYCLONE (BYPASS),
FLASK, FRONT HALF OF FILTER HOLDER

CONTAINER _____ mg

FILTER NUMBER _____

CONTAINER _____ mg

FRONT HALF SUBTOTAL _____ mg

BACK HALFIMPINGER CONTENTS AND WATER WASH OF
IMPINGERS, CONNECTORS, AND BACK
HALF OF FILTER HOLDER

CONTAINER _____ mg

ETHER-CHLOROFORM
EXTRACTION _____ mgACETONE WASH OF IMPINGERS, CONNECTORS,
AND BACK HALF OF FILTER HOLDER

CONTAINER _____ mg

BACK HALF SUBTOTAL _____ mg

TOTAL WEIGHT _____ mg

MOISTURE
 IMPINGERS
 FINAL VOLUME 283 ml
 INITIAL VOLUME 200 ml
 NET VOLUME 83 ml

 SILICA GEL
 FINAL WEIGHT 645.8 g _____ g _____ g
 INITIAL WEIGHT 631.7 g _____ g _____ g
 NET WEIGHT 14.1 g _____ g _____ g
EPA (Dur) 231
4/72

$$\text{cyclone} = \begin{array}{r} 7.2 \\ + 4.8 \\ \hline 12.0 \text{ ml} \end{array}$$

$$\text{wash} = \begin{array}{r} 449 \text{ ml} \\ + 25 \text{ ml} \\ \hline 474 \\ + 283 \\ \hline 757 \text{ ml} \end{array}$$

TOTAL MOISTURE _____ g

APPENDIX E

LABORATORY REPORT

This section presents the report on fluoride, ammonia, pH and P₂O₅ analysis which were performed by EPA.

SOURCE SAMPLE REQUEST & REPORT
(MUST BE FILLED OUT FOR EACH TEST RUN)

SAMPLING DATE 73 3 21
YR MO DAY

FIRST IDENT.
NO. USED 5 73 000511

LAST IDENT.
NO. USED 5 73 000512

TEST NO 73 FRT1

RUN NO F-1

INDUSTRY Phosphate Fertilizer
(USE TABLE A)

UNIT PROCESS OPERATION diammonium phosphate

RECD. 4-5-73
RCRD.

COMPANY Arco Chemical

AIR POLLUTION CONTROL scrubber

COPIES TO

ADDRESS St. Madison, Iowa

FUEL USED none

P. O. 6-13-73
LAB.

SAMPLING METHOD EPA Fluorides

☐ INLET ☒ OUTLET
GAS VOLUME SAMPLED 61.509
(METER VOL IN FT³)

FILED

IDENT NO	DESCRIPTION OF SAMPLE OR SAMPLE FRACTION	SAMPLE		ANALYSIS REQUESTED - GENERAL COMMENTS (APPROX CONCENTRATIONS - POSSIBLE INTERFERENCES ETC) (INDICATE SPECIFIC ANALYSIS ON BACKSIDE)
		WT (SOLID) MG	VOL (LIQUID) ML	
<u>5 73 000511</u>	<u>aprons contents & wash</u>	<u>N/A</u>	<u>250</u>	<u>Soluble and Insoluble fluorides (12.2 ml stock H₂O)</u>
<u>512</u>	<u>impinger contents, filter & wash</u>	<u>N/A</u>	<u>546 550</u>	<u>Soluble and Insoluble fluorides (66 ml stock H₂O)</u>
<u>76</u>				

COMMENTS:

SAMPLING CONTRACTOR Midwest Research Institute
(IF APPLICABLE)

PROJECT OFFICER Winton Kelly

REQUEST REVIEWED BY [Signature] 4/3/73

DATE OF REQUEST 4/3/73
EPA(DUR)245

DATE ANALYSIS REQUESTED 4/18/73

DATE OF REQUEST
(TO BE FILLED IN BY SSFAB)

Mark (x) for specific analysis
Mark (x) in block to left of Ident. No. when
requesting all analysis on that line

[illegible]

Comments:

Mark (x) for specific analysis requested

Ident No.	77	White flourides	Available flourides								
511	☒	0.5mg	☒ <0.06mg	☐	☐	☐	☐	☐	☐	☐	☐
512	☒	1.2mg	☒ <0.06mg	☐	☐	☐	☐	☐	☐	☐	☐
	☐		☐	☐	☐	☐	☐	☐	☐	☐	☐
	☐		☐	☐	☐	☐	☐	☐	☐	☐	☐
	☐		☐	☐	☐	☐	☐	☐	☐	☐	☐
	☐		☐	☐	☐	☐	☐	☐	☐	☐	☐
	☐		☐	☐	☐	☐	☐	☐	☐	☐	☐
	☐		☐	☐	☐	☐	☐	☐	☐	☐	☐
	☐		☐	☐	☐	☐	☐	☐	☐	☐	☐
	☐		☐	☐	☐	☐	☐	☐	☐	☐	☐
	☐		☐	☐	☐	☐	☐	☐	☐	☐	☐
	☐		☐	☐	☐	☐	☐	☐	☐	☐	☐
	☐		☐	☐	☐	☐	☐	☐	☐	☐	☐
Test		DMG + 1m	DMG + 1m								
thod		SPA DNS	SPA DNS								

ments:

MCBEE SYSTEMS P12352X

5
2.0 m
2.0 m

Mark (x) for specific analysis
Mark (x) in block to left of Ident. No. when
requesting all analysis on that line

Analysis Method: 1-NAA, 2-SSMS, 3-OES, 4-AA, 5-ASV, 6-XRF, and 7-other	Comments:
--	-----------

Mark (x) for specific analysis requested

Comments:

SOURCE SAMPLE REQUEST & REPORT
(MUST BE FILLED OUT FOR EACH TEST RUN)

MODEL SYSTEMS P22322A

SAMPLING DATE 73 3 22
YR MO DAY

FIRST IDENT. NO. USED S 73 000535

LAST IDENT. NO. USED S 73 000536

TEST NO. 73 FRT 1

RUN NO. F3

RECD. 4-5-73
RCRD.

INDUSTRY Phosphate Fertilizer
(USE TABLE A)

UNIT PROCESS OPERATION diomonum phosphate

COMPANY Arco Chemical

AIR POLLUTION CONTROL scrubber

ADDRESS St Madison, Iowa

FUEL USED none

SAMPLING METHOD EPA Fluorides

☐ INLET ☒ OUTLET
GAS VOLUME SAMPLED 69.865
(METER VOL IN FT³)

P. O. 6-13-73
LAB.

COPIES TO
FILED

IDENT NO	DESCRIPTION OF SAMPLE OR SAMPLE FRACTION	SAMPLE		ANALYSIS REQUESTED - GENERAL COMMENTS (APPROX CONCENTRATIONS - POSSIBLE INTERFERENCES ETC) (INDICATE SPECIFIC ANALYSIS ON BACKSIDE)
		WT (SOLID) MG	VOL (LIQUID) ML	
<u>573000535</u>	<u>cyclone contents & wash</u>	<u>N/A</u>	<u>250</u>	<u>Soluble & Insoluble fluorides (14.1 ml stock H₂O)</u>
<u>8 536</u>	<u>scrubber contents, filter & washes</u>	<u>N/A</u>	<u>647.660 ml</u>	<u>" " " (74 ml stock H₂O)</u>

COMMENTS: _____

SAMPLING CONTRACTOR Midwest Research Institute
(IF APPLICABLE)

PROJECT OFFICER Winston Kelly

REQUEST REVIEWED BY 4/3/73

DATE OF REQUEST 4/3/73
EPA(DUR)245

DATE ANALYSIS REQUESTED 4/12/73

DATE OF REQUEST _____
(TO BE FILLED IN BY SSFAB)

Mark (x) for specific analysis
Mark (x) in block to left of Ident. No. when
requesting all analysis on that line

Analysis Method: 1-NAA, 2-SSMS, 3-OES, 4-AA, 5-ASV, 6-XRF, and 7-other	Comments:
--	-----------

Mark (x) for specific analysis requested

Comments:

SOURCE SAMPLE REQUEST & REPORT
(MUST BE FILLED OUT FOR EACH TEST RUN)

SAMPLING DATE 73 3 22
YR MO DAY

FIRST IDENT. NO. USED 573 000546

LAST IDENT. NO. USED 573000548

TEST NO. 73 FRT 1

RUN NO. F4

INDUSTRY Phosphate Fertilizer
(USE TABLE A)

UNIT PROCESS OPERATION diammonium phosphate

RECD. 4-5-73
RCRD.

COMPANY Orco Chemical

AIR POLLUTION CONTROL scrubber

COPIES TO

ADDRESS St. Madison, Iowa

FUEL USED none

P. O. 6-13-73
LAB.

SAMPLING METHOD EPA - Fluorides

☐ INLET ☒ OUTLET
GAS VOLUME SAMPLED 72.459
(METER VOL IN FT³)

FILED

IDENT NO	DESCRIPTION OF SAMPLE OR SAMPLE FRACTION	SAMPLE		ANALYSIS REQUESTED - GENERAL COMMENTS (APPROX CONCENTRATIONS - POSSIBLE INTERFERENCES ETC) (INDICATE SPECIFIC ANALYSIS ON BACKSIDE)
		WT (SOLID) MG	VOL (LIQUID) ML	
573000546	cyclone contents & wash	N/A	250	Soluble & Insoluble fluorides (11.1 ml stock H ₂ O)
547	impinger contents, filter & washer	N/A	921.795	" " " (6.1 ml stock H ₂ O)
* 548	Water Blank			" " "

COMMENTS: * SAMPLE CONTAINER SPLIT, AND ENTIRE SAMPLE LOST DURING SHIPPING.

SAMPLING CONTRACTOR Midwest Research Institute
(IF APPLICABLE)

PROJECT OFFICER Winton Kelly

REQUEST REVIEWED BY 4/3/73

DATE OF REQUEST 4/3/73
EPA(DUR)245

DATE ANALYSIS REQUESTED 4/18/73

DATE OF REQUEST (TO BE FILLED IN BY SSFAB)

Mark (x) for specific analysis
Mark (x) in block to left of Ident. No. when
requesting all analysis on that line

Comments:

Mark (x) for specific analysis requested

Comments:

SOURCE SAMPLE REQUEST & REPORT

(MUST BE FILLED OUT FOR EACH TEST RUN)

SAMPLING DATE 73 3 23
YR MO DAY

FIRST IDENT. NO. USED 573 000 559

LAST IDENT. NO. USED 573 000 562

TEST NO. 73-FRT-1

RUN NO. F5

RECD. 4-5-73
RCRD.

INDUSTRY Phosphate Fertilizer
(USE TABLE A)

UNIT PROCESS OPERATION diammonium phosphate

COMPANY Arco Chemical

AIR POLLUTION CONTROL scrubber

ADDRESS Lt. Madison

FUEL USED none

P. O. 6-13-73

SAMPLING METHOD EPA Fluorides

☐ INLET ☒ OUTLET
GAS VOLUME SAMPLED 63,305
(METER VOL IN FT³)

LAB. 6-13-73

COPIES TO

FILED

IDENT NO	DESCRIPTION OF SAMPLE OR SAMPLE FRACTION	SAMPLE		ANALYSIS REQUESTED - GENERAL COMMENTS (APPROX CONCENTRATIONS - POSSIBLE INTERFERENCES ETC) (INDICATE SPECIFIC ANALYSIS ON BACKSIDE)
		WT (SOLID) MG	VOL (LIQUID) ML	
573000559	cyclone contents + wash	N/A	263	soluble + insoluble fluorides (120 ml stock H ₂ O)
560	impinger contents, filter, + washer	N/A	759.635	" " " (23 ml stock H ₂ O)
561	ammonia reagent blank	N/A	508	NH ₃
562	filter blank	N/A	N/A	soluble + insoluble fluorides

COMMENTS:

SAMPLING CONTRACTOR Michael Research Institute PROJECT OFFICER Winton Kelly REQUEST REVIEWED BY 4/3/73
(IF APPLICABLE)

DATE OF REQUEST 7/3/73 DATE ANALYSIS REQUESTED 7/8/73 DATE OF REQUEST (TO BE FILLED IN BY SSFAB)

Mark (x) for specific analysis
Mark (x) in block to left of Ident. No. when
requesting all analysis on that line

Analysis Method: 1-NAA, 2-SSMS, 3-OES, 4-AA, 5-ASV, 6-XRF, and 7-other	Comments:
--	-----------

Other Analysis - Use Table B to fill analysis requested (above each column)

Mark (x) for specific analysis requested

[illegible]

Comments:

Mark (x) for specific analysis
Mark (x) in block to left of Ident. No. when
requesting oil analysis on that line

Comments:

Mark (x) for specific analysis requested

Comments:

Mark (x) for specific analysis
Mark (x) in block to left of Ident. No. when
requesting all analysis on that line

Comments:

Mark (x) for specific analysis requested

Comments:

SOURCE SAMPLE REQUEST & REPORT
(MUST BE FILLED OUT FOR EACH TEST RUN)

SAMPLING DATE

73	3	22
YR	MO	DAY

FIRST IDENT.
NO. USED

573 000 525

LAST IDENT.
NO. USED

573 000 526

TEST NO 73-FRT-1

RUN NO A 3

RECD.

RCRD. { 4-5-73

INDUSTRY Phosphate Fertilizers
(USE TABLE A)

COMPANY Arco Chemical

ADDRESS St. Madison Iowa.

SAMPLING METHOD NH₃ EPA (H₂SO₄ scrubbing solution)

UNIT PROCESS OPERATION di ammonium phosphate

AIR POLLUTION CONTROL scrubber

FUEL USED none

☐ INLET ☒ OUTLET

GAS VOLUME SAMPLED 44.935
(METER VOL IN FT³)

COPIES TO

P. O.

LAB. } - 6-13-75

FILED

[illegible]

SAMPLING
CONTRACTOR Midwest Research Institute
(IF APPLICABLE)

PROJECT OFFICER Winton Kelly

REQUEST
REVIEWED BY LS 4/3/73

DATE OF REQUEST 4/3/73
EPA(DUR)245

DATE ANALYSIS REQUESTED 4/18/73

DATE OF REQUEST _____
(TO BE FILLED IN BY SSFAB)

Mark (x) for specific analysis
Mark (x) in block to left of Ident. No. when
requesting all analysis on that line

Comments:

SOURCE SAMPLE REQUEST & REPORT
(MUST BE FILLED OUT FOR EACH TEST RUN)

SAMPLING DATE 73 3 23
YR MO DAY

FIRST IDENT.
NO. USED 573 000 557

LAST IDENT.
NO. USED 573 000 558

TEST NO. 73 FRT 1

REC'D. RUN NO. A4
RCRD. 4-5-73

INDUSTRY Phosphate Fertilizer
(USE TABLE A)

UNIT PROCESS OPERATION Ammonium phosphate

COMPANY Acro Chemical

AIR POLLUTION CONTROL scrubber

ADDRESS St. Madison, Iowa

FUEL USED none

P. O. 6-13-73
LAB.

SAMPLING METHOD EPA ammonia

☐ INLET ☒ OUTLET
GAS VOLUME SAMPLED 42.686
(METER VOL IN FT³)

FILED

IDENT NO	DESCRIPTION OF SAMPLE OR SAMPLE FRACTION	SAMPLE		ANALYSIS REQUESTED - GENERAL COMMENTS (APPROX CONCENTRATIONS - POSSIBLE INTERFERENCES ETC) (INDICATE SPECIFIC ANALYSIS ON BACKSIDE)
		WT (SOLID) MG	VOL (LIQUID) ML	
<u>573000557</u>	<u>filter</u>	<u>N/A</u>	<u>N/A</u>	<u>storage</u>
<u>26 558</u>	<u>impinger contents, & washer</u>	<u>N/A</u>	<u>595 496</u>	<u>ammonia (62 ml stock H₂O solution)</u>

COMMENTS:

SAMPLING CONTRACTOR Midwest Research Institute
(IF APPLICABLE)

PROJECT OFFICER Winton Kelly

REQUEST REVIEWED BY [Signature] 4/5/73

DATE OF REQUEST 4/3/73
EPA(DUR)245

DATE ANALYSIS REQUESTED 4/18/73

DATE OF REQUEST
(TO BE FILLED IN BY SSFAB)

Mark (x) for specific analysis
Mark (x) in block to left of Ident. No. when
requesting all analysis on that line

Analysis Method: 1-NAA, 2-SIMS, 3-OES, 4-AA, 5-ASV, 6-XRF, and 7-other	Comments:
--	-----------

[illegible]

Comments:

SOURCE SAMPLE REQUEST & REPORT

(MUST BE FILLED OUT FOR EACH TEST RUN)

SAMPLING DATE

73 3 21
YR MO DAY

FIRST IDENT.
NO. USED

573 000503

LAST IDENT.
NO. USED

573 000510

TEST NO. 73-FRT-1

RUN NO. 1

INDUSTRY PHOSPHATE FERTILIZER
(USE TABLE A)

UNIT PROCESS OPERATION DIAMMONIUM PHOSPHATE

COMPANY ARCO CHEMICAL

AIR POLLUTION CONTROL SCRUBBER

ADDRESS FT. MADISON IOWA

FUEL USED NONE

SAMPLING METHOD EXTRACTOR Grab

☐ INLET ☒ OUTLET
GAS VOLUME SAMPLED
(METER VOL IN FT³)

RECD. }
RCRD. } 4-5-73

COPIES TO

P. O. } 6-13-73
LAB. }

FILED

IDENT NO	DESCRIPTION OF SAMPLE OR SAMPLE FRACTION	SAMPLE		ANALYSIS REQUESTED - GENERAL COMMENTS (APPROX CONCENTRATIONS - POSSIBLE INTERFERENCES ETC) (INDICATE SPECIFIC ANALYSIS ON BACKSIDE)
		WT (SOLID) MG	VOL (LIQUID) ML	
573 000503	venturi scrubber inlet liquor } ~ 26% phosphoric acid	N/A	N/A	total fluorides, pH
94 504	venturi scrubber outlet liquor }	N/A	N/A	total fluorides, ammonia, pH
* 505	gypsum pond water	N/A	N/A	total fluorides, pH, P ₂ O ₅
506	reactor granulator afterscrubber outlet liquor	N/A	N/A	total fluorides, ammonia
507	boiler afterscrubber outlet liquor	N/A	N/A	total fluorides, ammonia
+ 508	Dryer afterscrubber outlet liquor	N/A	N/A	total fluorides, ammonia
509	Fuel acid (54% phosphoric acid)	N/A	N/A	total fluorides, P ₂ O ₅
510	DAP product	N/A	N/A	total fluorides, P ₂ O ₅ , NH ₃
COMMENTS: * SAMPLE CONTAINER SPLIT, AND ENTIRE SAMPLE LOST DURING SHIPPING. + SAMPLE MISSING				

SAMPLING

CONTRACTOR Midwest Research Institute
(IF APPLICABLE)

PROJECT OFFICER Winston Kelly

REQUEST

REVIEWED BY 4/3/73

DATE OF REQUEST 4/3/73

DATE ANALYSIS REQUESTED 4/18/73

DATE OF REQUEST

EPA(CUR)245

(TO BE FILLED IN BY SSFAB)

Mark (x) for specific analysis
Mark (x) in block to left of Ident. No. when
requesting all analysis on that line o

Analysis Method: 1-NAA, 2-SSMS, 3-OES, 4-AA, 5-ASV, 6-XRF, and 7-other	Comments:
--	-----------

her Analysis - Use Table 8 to fill analysis requested (above each column)

Mark (x) for specific analysis requested

Ident No.	Total Sulfurides	P ₂ O ₅	pH	Ammonia						
503	X 17.3 g/L		X 0.52							
504	X 13.8 g/L		X 2.93	X 100.8 g/L						
505	X SAMPLE GONE	X SAMPLE GONE	X SAMPLE GONE							
506	X 1.79 g/L			X 592.6 mg/L						
507	X 1.8 g/L			X 504.1 mg/L						
508	X SAMPLE GONE			X SAMPLE GONE						
509	X 12.1 g/L	X 850 g/L								
510	X 26.4 mg/gm	X 520 mg/gm		X 211.2 mg/gm						
Dist	DMG + 3/21	DMG + 9/21	3/11/21	DMG + 8/21						
thod	SPADNS	AMMONIUM MOLYBDATE		KJELDAHL DISTILLATION						

ments:

SOURCE SAMPLE REQUEST & REPORT (MUST BE FILLED OUT FOR EACH TEST RUN)

SAMPLING DATE 73 3 21
YR MO DAY

FIRST IDENT.
NO. USED 5-73-000515

LAST IDENT.
NO. USED 5-73-000522

TEST NO. 73-FRT-1

RUN NO. 2

RECD. }
RCRD. } 4-5-73

INDUSTRY Phosphate Fertilizer
(USE TABLE A)

UNIT PROCESS OPERATION diammonium phosphate

COMPANY Arco Chemical

AIR POLLUTION CONTROL scrubber

COPIES TO

ADDRESS St. Madison Iowa

FUEL USED none

SAMPLING METHOD [REDACTED]

☐ INLET ☒ OUTLET
GAS VOLUME SAMPLED
(METER VOL IN FT³)

P. O. }
LAB. } 6-13-73

FILED

IDENT NO	DESCRIPTION OF SAMPLE OR SAMPLE FRACTION	SAMPLE		ANALYSIS REQUESTED - GENERAL COMMENTS (APPROX CONCENTRATIONS - POSSIBLE INTERFERENCES ETC) (INDICATE SPECIFIC ANALYSIS ON BACKSIDE)
		WT (SOLID) MG	VOL (LIQUID) ML	
573 000515	venturi scrubber inlet liquor } 26% phosphoric acid	N/A	N/A	total fluorides, pH
516	venturi scrubber outlet liquor }	N/A	N/A	" " ammonia, pH
96 517	gypsum pond water	N/A	N/A	total fluorides, pH, P ₂ O ₅
518	Reactor granulated after scrubber liquor out	N/A	N/A	total fluorides, ammonia
519	cooler after scrubber liquor out	N/A	N/A	" "
520	dryer after scrubber liquor out	N/A	N/A	" "
521	feed acid (54% phosphoric acid)	N/A	N/A	total fluorides, P ₂ O ₅
522	DAP product (diammonium phosphate)	N/A	N/A	total fluorides, P ₂ O ₅ , ammonia
COMMENTS:				

SAMPLING
CONTRACTOR Midwest Research Institute
(IF APPLICABLE)

PROJECT OFFICER Winters Kelly

REQUEST
REVIEWED BY Gib 4/3/73

DATE OF REQUEST 4/3/73
EPA(DUR)245

DATE ANALYSIS REQUESTED 4/18/73

DATE OF REQUEST
(TO BE FILLED IN BY SSFAB)

Mark (x) for specific analysis.
Mark (x) in block to left of Ident. No. when
requesting all analysis on that line

[illegible]

Comments:

Mark (x) for specific analysis requested

[illegible]

connects:

SAMPLING DATE	73	3	22
	YR	MO	DAY

LAST IDENT. 373 000 534
NO. USED

RUN NO 3

RECD. }
RCRD. } 4-5-73

UNIT PROCESS OPERATION diammonium phosphate

AIR POLLUTION CONTROL scrubber

FUEL USED none

COPIES TO

☐ INLET ☒ OUTLET
GAS VOLUME SAMPLED _____
(METER VOL IN FT³)

P. O. 6-13-73
LAE.

FILED

SAMPLING CONTRACTOR Midwest Research Institute PROJECT OFFICER Winton Kelly
(IF APPLICABLE)

REQUEST
REVIEWED BY 4/3/73

DATE OF REQUEST 4/3/73 DATE ANALYSIS REQUESTED 4/18/73
EPA(DUR)245

DATE OF REQUEST _____
(TO BE FILLED IN BY SSFAB)

Mark (x) for specific analysis
Mark (x) in block to left of Ident. No. when
requesting all analysis on that line

Analysis Method: 1-NAA, 2-SSMS, 3-OES, 4-AA, 5-ASV, 6-XRF, and 7-other Comments:

her Analysis - Use Table B to fill analysis requested (above each column)

Mark (x) for specific analysis requested

Ident No.	total fluorides	P ₂ O ₅	pH	ammoniac					
66 527	X 25.6 gm/L		X 0.28						
528	X 6.0 gm/L		X 5.38	X 107.5 gm/L					
529	X 2.0 gm/L	X 2.8 gm/L	X 1.75						
530	X 1.6 gm/L			X 487.1 mg/L					
531	X 1.7 gm/L			X 1.3 gm/L					
532	X 1.7 gm/L			X 580 mg/L					
533	X 14.5 gm/L	X 790 gm/L							
534	X 24.4 mg/gm	X 500 mg/gm		X 228.2 mg/L	?				
dist	DMG + Jm	DMG + Jm	gmaeb	DMG + Jm					
thos	SPADIS	Ammonium Molybdate		KJELDAHL	DISTILLATION				

ATTENTION:

SOURCE SAMPLE REQUEST & REPORT

(MUST BE FILLED OUT FOR EACH TEST RUN)

SAMPLING DATE 73 3 22
YR MO DAY

FIRST IDENT.
NO. USED 573 0005 37

LAST IDENT.
NO. USED 573 000545

TEST NO. 73 FRT 1

RUN NO. 4
RECD. 4-5-73
RCRD. 4-5-73

INDUSTRY Phosphate Fertilizer
(USE TABLE A)

UNIT PROCESS OPERATION diammonium phosphate

COMPANY Oreo Chemical

AIR POLLUTION CONTROL scrubber

ADDRESS St Madison, Iowa

FUEL USED none

COPIES TO

SAMPLING METHOD Grab

☐ INLET ☐ OUTLET
GAS VOLUME SAMPLED
(METER VOL IN FT³)

P. O. 6-13-73
LAB. 6-13-73

FILED

IDENT NO	DESCRIPTION OF SAMPLE OR SAMPLE FRACTION	SAMPLE		ANALYSIS REQUESTED - GENERAL COMMENTS (APPROX CONCENTRATIONS - POSSIBLE INTERFERENCES ETC) (INDICATE SPECIFIC ANALYSIS ON BACKSIDE)
		WT (SOLID) MG	VOL (LIQUID) ML	
573 000537	venturi scrubber inlet liquor } 21% phosphoric acid	N/A	N/A	total fluorides, pH
*538	venturi scrubber outlet liquor			total fluorides, ammonia, pH
100 539	gypsum pond water	N/A	N/A	total fluorides, pH, P ₂ O ₅
540	farm run-off water	N/A	N/A	" " " "
541	Reactor granulator after scrubber outlet liquor	N/A	N/A	total fluorides, ammonia
542	Cooler after scrubber outlet liquor	N/A	N/A	" " "
543	dryer after scrubber outlet liquor	N/A	N/A	" " "
544	feed acid (54% phosphoric acid)	N/A	N/A	total fluorides, P ₂ O ₅
545	DAP product	N/A	N/A	total fluorides, P ₂ O ₅ , ammonia

COMMENTS: * SAMPLE CONTAINER SPLIT, AND ENTIRE SAMPLE LOST DURING SHIPPING.

SAMPLING CONTRACTOR Midwest Research Institute
(IF APPLICABLE)

PROJECT OFFICER Winton Kelly

REQUEST REVIEWED BY 4/12/73

DATE OF REQUEST 4/3/73
EPA(DUR)245

DATE ANALYSIS REQUESTED 4/18/73

DATE OF REQUEST
(TO BE FILLED IN BY SSFAB)

Mark (x) for specific analysis
Mark (x) in block to left of Ident. No. when
requesting all analysis on that line

Analysis Method: 1-NAA, 2-SSMS, 3-OES, 4-AA, 5-ASV, 6-XRF, and 7-other	Comments:
--	-----------

Mark (x) for specific analysis requested

Comments:

SOURCE SAMPLE REQUEST & REPORT

(MUST BE FILLED OUT FOR EACH TEST RUN)

SAMPLING DATE 73 3 23
 YR MO DAY

FIRST IDENT. NO. USED 5 73 000549

LAST IDENT. NO. USED 5 73 000556

TEST NO. 73-FRT-1

RUN NO. 5

RECD. 1-5-73

RCD. 1-5-73

COPIES TO

P. O. 6-13-73
 LAB.

FILED

INDUSTRY Phosphate Fertilizer
 (USE TABLE A)

UNIT PROCESS OPERATION diammonium phosphate

COMPANY Arco Chemical

AIR POLLUTION CONTROL scrubber

ADDRESS St. Madison, Iowa

FUEL USED none

SAMPLING METHOD Grab

☐ INLET ☐ OUTLET
 GAS VOLUME SAMPLED
 (METER VOL IN FT³)

IDENT NO	DESCRIPTION OF SAMPLE OR SAMPLE FRACTION	SAMPLE		ANALYSIS REQUESTED - GENERAL COMMENTS (APPROX CONCENTRATIONS - POSSIBLE INTERFERENCES ETC) (INDICATE SPECIFIC ANALYSIS ON BACKSIDE)
		WT (SOLID) MG	VOL (LIQUID) ML	
573000549	venturi scrubber inlet liquor } -26%	N/A	N/A	total fluorides, pH
102 550	venturi scrubber outlet liquor } phosphate	N/A	N/A	total fluorides, ammonia, pH
551	pond water	N/A	N/A	total fluorides, pH, P ₂ O ₅
552	Rocter granulator after scrubber outlet liquor	N/A	N/A	total fluorides, ammonia
553	cooler after scrubber outlet liquor	N/A	N/A	" " "
554	dryer after scrubber outlet liquor	N/A	N/A	" " "
555	feed acid (54%)	N/A	N/A	total fluorides, P ₂ O ₅
556	DAP product	N/A	N/A	total fluorides, P ₂ O ₅ , ammonia

COMMENTS:

SAMPLING CONTRACTOR Midwest Research Institute
 (IF APPLICABLE)

PROJECT OFFICER Winton Kelly

REQUEST REVIEWED BY 4/3/73

DATE OF REQUEST 4/3/73
 EPA(DUR)245

DATE ANALYSIS REQUESTED 4/18/73

DATE OF REQUEST
 (TO BE FILLED IN BY SSFAB)

Mark (x) for specific analysis
Mark (x) in block to left of Ident. No. when
requesting all analysis on that line

[illegible]

Comments:

Mark (x) for specific analysis requested

[illegible]

Comments:

APPENDIX F

TEST LOG

Table F-I presents the actual time during which each sampling was done.

TABLE F-1

SAMPLING LOG

<u>Run</u>	<u>Location</u>	<u>Port</u>	<u>Pollutant</u>	<u>Date</u>	<u>Time</u>	<u>Elapsed</u>
					<u>Began-Ended</u>	<u>Time (min)</u>
F-1A	Stack	1	Temperature and velocity	3-20-73	15:00-15:20	20
F-1	Stack	1	Fluoride	3-21-73	10:52-11:25	33
1	"	2	Fluoride	"	11:44-12:35	51
	"	3	CO, CO ₂ , O ₂	"	11:50-12:20	30
	"	3	Fluoride	"	12:45-13:15	30
	"	4	Fluoride	"	13:25-13:55	30
NH ₃ -1	"	4	Ammonia	"	10:58-11:58	60
F-1, NH ₃ -1	Various	-	Liquid/Solid	"	11:00-13:45	165
F-2	Stack	1	Fluoride	"	16:04-16:34	30
F-2	"	2	Fluoride	"	16:45-17:15	30
F-2	"	3	CO, CO ₂ , O ₂	"	16:20-16:50	30
F-2	"	3	Fluoride	"	17:23-17:53	30
F-2	"	4	Fluoride	"	18:00-18:30	30
NH ₃ -2	"	4	Ammonia	"	16:10-17:10	60
F-2, NH ₃ -2	Various	-	Liquid/Solid	"	16:10-18:10	120
F-3	Stack	1	Fluoride	3-22-73	10:04-10:34	30
F-3	"	2	Fluoride	"	10:44-11:14	30
F-3	"	1	CO, CO ₂ , O ₂	"	11:08-11:38	30
F-3	"	3	Fluoride	"	11:24-11:54	30
F-3	"	4	Fluoride	"	12:13-12:43	30
NH ₃ -3	"	4	Ammonia	"	11:01-12:01	60
F-3, NH ₃ -3	Various	-	Liquid/Solid	"	10:10-12:10	120
F-4	Stack	1	Fluoride	"	15:20-15:50	30
F-4	"	2	Fluoride	"	15:58-16:28	30
F-4	"	3	Fluoride	"	16:38-17:08	30
F-4	"	4	CO, O ₂ , CO ₂	"	15:34-16:04	30
F-4	"	4	Fluoride	"	17:16-17:46	30
F-4	Various	-	Solid/liquid	"	15:30-17:30	120
F-5	Stack	1	Fluoride	3-23-73	09:39-10:09	30
F-5	"	2	Fluoride	"	10:19-10:49	30
F-5	"	3	CO, CO ₂ , O ₂	"	10:05-10:35	30
F-5	"	3	Fluoride	"	10:58-11:28	30
F-5	"	4	Fluoride	"	11:38-12:08	30
NH ₃ -4	"	4	Ammonia	"	09:48-10:48	60
F-5, NH ₃ -4	Various	-	Liquid/Solid	"	09:45-12:00	135

APPENDIX G

PROJECT PARTICIPANTS AND TITLES

<u>Name</u>	<u>Title</u>
Paul Constant	Program Manager
Pat Shea	Project Chief
Reid Flippin	Testing Engineer Laboratory Technician
Henry Moloney	Process Sampler
Bill Maxwell	Engineering Technician
Mike Bechtold	Testing Engineer and Engineering Technician
Bill Cunningham	Laboratory Technician Engineering Technician
Christine Guenther	Programmer