Stationary Source Compliance Series

\$EPA

Utility FGD Survey October 1983-September 1984

Volume 2: Design Performance Data For Operating FGD Systems (Part 1)

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Alabama Electric, Tombigbee 2 through Montana Power, Colstrip 2

M. T. Melia, R. S. McKibben, and B. W. Pelsor

PEDCo Environmental, Inc. 11499 Chester Road Cincinnati, Ohio 45246

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EPA Project Manager: John Busik EPA Work Assignment Manager: Sonya M. Stelmack

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NOTICE

The data in this information transfer document are supplied voluntarily by utility representatives, flue gas desulfurization (FGD) system suppliers and designers, regulatory agencies, and others. The accuracy or completeness of the information contained herein is not warranted by the Stationary Source Control Division of EPA or the designated contractor. Portions of the work upon which this publication is based were performed pursuant to Contract Nos. RP982-32 (Electric Power Research Institute) and 68-02-3173 (Environmental Protection Agency).

A project summary will be distributed to organizations and individuals indicating a specific interest in the field of FGD technology. Interested parties can be added to the Project Summary mailing list by contacting Carolyn Fowler at the Industrial Environmental Research Laboratory (919/541-2915) or the secretary of the Emission and Effluent Technology Branch of the EPA (919/541-2578). Copies of preceding issues of this report through December 1981 can be purchased from the National Technical Information Service, Springfield, Virginia 22161, (703) 487-4650. Succeeding issues of this report can be purchased from the Electric Power Research Institute Research Reports Center, P.O. Box 50490, Palo Alto, California 94303, (415) 965-4081.

This report summarizes the FGD system design and performance data contained in a computerized data base known as the Flue Gas Desulfurization Information System (FGDIS). Access to the FGDIS is available through the National Technical Information Service (NTIS) for a nonprofit user's fee. Users also have access to additional design and performance data stored within the data base that cannot conveniently be printed in this report. Direct access to the data base affords analyses of the data (e.g., averages, maxima, minima, and standard deviations of various parameters), the use of simple mathematical functions, the capability of virtually unlimited data cross-referencing, and data tabulation to fit the user's individual information needs. An FGDIS users manual is available from NTIS (NTIS No. PB 83 146 209).

Requests for further information concerning the FGDIS and periodic FGDIS training seminars should be directed to Michael Melia or Skip Jones, PEI Associates, Inc. (513/782-4700). Information concerning access to the FGDIS can be obtained from Walter Finch, NTIS, 5285 Port Royal Road, Springfield, Virginia 22161 (703/487-4808).

USE OF THIS REPORT

This report is the first fully compiled edition since the July 1982-March 1983 issue released in April 1984, which contains more complete design and performance data since the FGS system startup dates. This report supersedes all previous issues. Volume 1 includes several categorical summaries of key data and the appendix sections. Volume 2, Parts 1 and 2 contain all available design and performance data for operational FGD systems (Section 13).

The Executive Summary contains the number and capacity of FGD systems as of the end of December 1984, future (December 1993) projections of controlled and uncontrolled generating capacity, and unit-by-unit summaries of status changes (e.g., contract awarded, under construction, or operational) and performance and status highlights for the period.

Appendix sections include definitions, a table of unit notation and simplified process flow diagrams, as well as data on terminated FGD systems, particle scrubbers and Japanese FGD systems.

ABSTRACT

The Utility FGD Survey report, which is generated by a computerized data base system, represents a survey of operational and planned domestic utility flue gas desulfurization (FGD) systems. The three volume set summarizes information contributed by the utility industry, system and equipment suppliers, system designers, research organizations, and regulatory agencies. The data cover system design, fuel characteristics, operating history, and actual system performance. Also included is a unit-by-unit discussion of problems and solutions associated with the boilers, scrubbers, and FGD systems.

The development status (operational, under construction, or in the planning stages), system supplier, process, waste disposal practice, and regulatory class are tabulated alphabetically by utility company. Simplified process flow diagrams of FGD systems, definitions, and a glossary of terms are attached to the report. Current data for domestic FGD systems show 124 systems in operation, 25 systems under construction, and 68 systems planned. The current FGD-controlled capacity in the United States is 47,255 MW.

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SECTION 13

DESIGN AND PERFORMANCE FOR OPERATIONAL DOMESTIC FGD SYSTEMS

ALABAMA ELECTRIC, TOMBIGBEE 2
THROUGH
MONTANA POWER, COLSTRIP 2

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COMPANY NAME	ALABAMA ELECTRIC
PLANT NAME	TOMBIGBEE
UNIT NUMBER	2
CITY	LEROY
STATE	
REGULATORY CLASSIFICATION	ALABAMA
	D (7 (300 LD (MMDTL))
PARTICULATE EMISSION LIMITATION - NG/J .	43. (.100 LB/MMBTU)
SO2 EMISSION LIMITATION - NG/J	516. (1.200 LB/MMBTU)
NOX EMISSION LIMITATION - NG/J	301. (.700 LB/HMBTU)
NET PLANT GENERATING CAPACITY - MM	525
GROSS UNIT GENERATING CAPACITY - MW	255
NET UNIT GENERATING CAPACITY W/FGD - MW	235
NET UNIT GENERATING CAPACITY WO/FGD ~ MW	243
EQUIVALENT SCRUBBED CAPACITY - MW	179
** UNIT DATA - BOILER AND STACK	
BOILER SUPPLIER	RILEY STOKER
BOILER TYPE	PULVERIZED COAL
BOILER SERVICE LOAD	BASE
DESIGN BOILER FLUE GAS FLOW - CU.M/S	449.72 (953000 ACFM)
BOILER FLUE GAS TEMPERATURE - C	449.72 (953000 ACFM) 143.9 (291 F)
STACK HEIGHT - M	122. (400 FT)
STACK SHELL	CONCRETE
STACK TOP DIAMETER - M	5.0 (16.5 FT)
	(2010 1 1 7
** FUEL DATA	
FUEL TYPE	COAL
FUEL GRADE	BITUMINOUS
AVERAGE HEAT CONTENT - J/G	26572. (11424 BTU/LB)
RANGE HEAT CONTENT - BTU/LB	10000-11000
AVERAGE ASH CONTENT - %	14.73
RANGE ASH CONTENT - %	
	15-18
AVERAGE MOISTURE CONTENT - %	6.64
RANGE MOISTURE CONTENT %	3.0-20.0
AVERAGE SULFUR CONTENT - %	1.61
RANGE SULFUR CONTENT - X	1.5-1.75
RANGE SULFUR CONTENT - X AVERAGE CHLORIDE CONTENT - X RANGE CHLORIDE CONTENT - X	.04
RANGE CHLORIDE CONTENT - %	****
*** PARTICLE CONTROL	
WE MESHANTON COLLEGEOR	
** MECHANICAL COLLECTOR	_
NUMBER	0
TYPE	NONE
** ESP	
NUMBER	1
NUMBER OF SPARES	0
TYPE	HOT SIDE
SUPPLIER	RESEARCH-COTTRELL
INLET FLUE GAS CAPACITY - CU.M/S	449.7 (953000 ACFM)
INLET FLUE GAS TEMPERATURE - C	143.9 (291 F)
PRESSURE DROP - KPA	.1 (1. IN-H2O)
PARTICLE REMOVAL EFFICENCY - %	99.5
** PARTICLE SCRUBBER	
NUMBER	0
GENERIC TYPE	NONE
SPECIFIC TYPE	N/A
TRADE NAME/COMMON NAME	N/A
SHELL GENERIC MATERIAL	N/A
SHELL SPECIFIC MATERIAL	N/A
LINER GENERIC MATERIAL	N/A
LINER SPECIFIC MATERIAL	N/A N/A
GAS CONTACTING DEVICE TYPE	N/A

*** FGD SYSTEM

ALABAMA ELECTRIC: TOMBIGBEE 2 (CONT.)

```
** GENERAL DATA
    SALEABLE PRODUCT/THROWAWAY PRODUCT
                                              THROWAWAY PRODUCT
    SO2 REMOVAL MODE
                                              WET SCRUBBING
    PROCESS TYPE
                                              1 TMESTONE
    PROCESS ADDITIVES
                                              NONE
    SYSTEM SUPPLIER
                                              PEABODY PROCESS SYSTEMS
    A-E FIRM
                                               BURNS & MCDONNELL
    DEVELOPMENT LEVEL
                                               FULL SCALE
    NEW/RETROFIT
                                              NEW
    UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.50
                                              59.50
    UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
    ENERGY CONSUMPTION - %
                                                  3.1
    CURRENT STATUS
    COMMERCIAL START-UP
                                               9/78
    INITIAL START-UP
                                                9/78
    CONTRACT AWARDED
                                               8/75
** DESIGN AND OPERATING PARAMETERS
                                            1.48
29075.0
                                                1.48
    DESIGN COAL SULFER CONTENT %
    DESIGN COAL HEAT CONTENT - J/G
DESIGN COAL ASH CONTENT - X
                                                             ( 12500 BTU/LB)
                                               10.00
                                                 8.00
    DESIGN MOISTURE CONTENT - %
    DESIGN CHLORIDE CONTENT - X
                                                  .04
                                                        ( 50000 SQ FT)
    SPACE REQUIREMENTS SQ M
                                               4645.0
    OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                72.0
** QUENCHER/PRESATURATOR
    NUMBER
                                               2
                                               SPRAY
    TYPE
                                              127.41 ( 270000 ACFM)
143.9 ( 291 F)
35. ( 550 GPM)
    INLET GAS FLOW - CU. M/S
    INLET GAS TEMPERATURE - C
                                         35.
High Alloy
    LIQUID RECIRCULATION RATE - LITERS/S
    CONSTRUCTION MATERIAL GENERIC TYPE
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              NICKEL BASE/CHROMIUM-IRON-COPPER-MOLYBDENUM
** ABSORBER
    NUMBER
                                               2
    NUMBER OF SPARES
                                               SPRAY TOWER
    GENERIC TYPE
    SPECIFIC TYPE
                                               OPEN COUNTERCURRENT SPRAY
    TRADE NAME/COMMON TYPE
                                              N/A
    SUPPLIER
                                               PEABODY PROCESS SYSTEMS
    DIMENSIONS - FT
                                               24.0 DIA X 90.0
    SHELL GENERIC MATERIAL
                                               CARBON STEEL
    SHELL SPECIFIC MATERIAL
                                              AISI 1110
    SHELL MATERIAL TRADE NAME/COMMON TYPE
    LINER GENERIC MATERIAL
                                               DECANTO
    LINER SPECIFIC MATERIAL
                                               GLASS FLAKE-FILLED POLYESTER
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                               RESISTA-FLAKE 1151
    GAS CONTACTING DEVICE TYPE
                                               NONE
    NUMBER OF CONTACTING ZONES
                                               6
                                                            (19980 GPM)
( 74.0 GAL/1000 ACF)
    LIQUID RECIRCULATION RATE LITER/S
                                              1259.
                                              9.9
1.0
3.0
    L/G RATIO - L/CU.M
                                                             ( 4.0 IN-H20)
( 10.0 FT/S)
    GAS-SIDE PRESSURE DROP - KPA
                                              3.0
127.41
-4.4
    SUPERFICAL GAS VELOCITY M/SEC
    INLET GAS FLOW CU. M/S
                                                             ( 270000 ACFM)
    INLET GAS TEMPERATURE - C
                                                             ( 130 F)
    SO2 REMOVAL EFFICIENCY - %
                                                 85.0
                                                 99.5
    PARTICLE REMOVAL EFFICENCY - %
** MIST ELIMINATOR
    PRE-MIST ELIMINATOR/MIST ELIMINATOR PRIMARY COLLECTOR
    NUMBER PER SYSTEM
                                                2
    NUMBER OF SPARES PER SYSTEM
                                                0
    NUMBER PER MODULE
                                               IMPINGEMENT
    GENERIC TYPE
                                               BAFFLE
    SPECIFIC TYPE
                                              CLOSED VANE
    TRADE NAME/COMMON TYPE
                                              SHAH-HEIL
    MANUFACTUPER
                                               HORIZONTAL
    CONFIGURATION
```

ALABAMA ELECTRIC: TOMBIGBEE 2 (CONT.) NUMBER OF STAGES 1 NUMBER OF PASSES PER STAGE 1 FREEBOARD DISTANCE - M (4.0 FT) 1.22 PRESSURE DROP - KPA (.5 IN-H2O) . 1 SUPERFICAL GAS VELOCITY - M/S 3.0 (10.0 FT/S) CONSTRUCTION MATERIAL GENERIC TYPE ORGANIC CONSTRUCTION MATERIAL SPECIFIC TYPE POLYPHENYLENE WASH WATER SOURCE MAKEUP WASH FREQUENCY INTERMITTENTLY ** REHEATER NUMBER 1 GENERIC TYPE **BYPASS** SPECIFIC TYPE COLD SIDE TRADE NAME/COMMON TYPE N/A LOCATION ABSORBER OUTLET DUCT PERCENT GAS BYPASSED - AVG 30.0 TEMPERATURE INCREASE - C 48 F) 26.7 (INLET FLUE GAS FLOW RATE - CU. M/S 134.92 (285900 ACFM) INLET FLUE GAS TEMPERATURE - C 143.9 (291 F) OUTLET FLUE GAS TEMPERATURE - C 81.1 (178 F) CONSTRUCTION MATERIAL GENERIC TYPE HIGH ALLOY CONSTRUCTION MATERIAL SPECIFIC TYPE NICKEL BASE/CHROMIUM-IRON-MOLYBDENUM ** FANS NUMBER 2 NUMBER OF SPARES O CENTRIFUGAL DESTGN SUPPLIER PEABODY PROCESS SYSTEMS **FUNCTION** UNIT APPLICATION FORCED DRAFT DRY SERVICE FLUE GAS FLOW RATE - CU.M/S 225.10 (477000 ACFM) FLUE GAS TEMPERATURE - C 143.9 (291 F) CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL ** DAMPERS NUMBER 2 **FUNCTION** SHUT-OFF GENERIC TYPE GUILLOTINE MANUFACTURER MOSSER CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL CONSTRUCTION MATERIAL SPECIFIC TYPE NR LINER GENERIC MATERIAL TYPE HIGH ALLOY LINER SPECIFIC MATERIAL TYPE NICKEL BASE/CHROMIUM-IRON-COPPER-MOLYBDENUM ** DAMPERS NUMBER 2 **FUNCTION** SHUT-OFF GENERIC TYPE GUILLOTINE MANUFACTURER MOSSER CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL CONSTRUCTION MATERIAL SPECIFIC TYPE ND LINER GENERIC MATERIAL TYPE HIGH ALLOY NICKEL BASE/CHROMIUM-IRON-COPPER-MOLYBDENUM LINER SPECIFIC MATERIAL TYPE ** DAMPERS NUMBER 2 CONTROL **FUNCTION** GENERIC TYPE LOUVER MANUFACTURER MOSSER CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL CONSTRUCTION MATERIAL SPECIFIC TYPE ΝR NONE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE N/A ** DUCTWORK LOCATION SCRUBBER INLET CONFIGURATION RECTANGULAR DIMENSIONS 7 FT X 12 FT SHELL GENERIC MATERIAL TYPE CARBON STEEL

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ALABAMA ELECTRIC: TOMBIGBEE 2 (CONT.)
```

SHELL SPECIFIC MATERIAL TYPE AISI 1110
LINER GENERIC MATERIAL TYPE NONE
LINER SPECIFIC MATERIAL TYPE N/A

** DUCTWORK

LOCATION
CONFIGURATION
DIMENSIONS
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

SCRUBBER OUTLET TO STACK
RECTANGULAR
5.5 FT X 12 FT AND 13 FT X 16 FT
CARBON STEEL
AISI 1110
ORGANIC
FLUOROELASTOMER

(6.2 TPH)

** REAGENT PREPARATION EQUIPMENT

FUNCTION WET BALL MILL
DEVICE COMPARTMENTED
DEVICE TYPE NR
MANUFACTURER KENNEDY VAN SAUN
NUMBER 1
FULL LOAD DRY FEED CAPACITY - M.TONS/HR 9.1 (10 TPH)

PRODUCT QUALITY - % SOLIDS 35.0

** TANKS

SERVICE NUMBER

ABSORBER RECYCLE 1
MIST ELIMINATOR WASH 1
LIMESTONE SLURRY STORAGE 1
HYDROCLONE UNDERFLOW ****
MILL RECYCLE SUMP 1
WASTE SLURRY SUMP 1

** PUMPS

SERVICE NUMBER

ABSORBER RECIRCULATION 6
LIMESTONE MILL SLURRY RECIRCULATION 2
LIMESTONE SLURRY FEED 2
MIST ELIMINATOR WASH 3
WASTE SLURRY 2
SUPERNATE RETURN 1

** SOLIDS CONCENTRATING/DEWATERING

DEVICE NONE

*** SLUDGE

FULL LOAD SLUDGE QUANTITY - M.TONS/HR (DRY) 5.6
% CASO3 - DRY 17.0
% CASO4 DRY 70.0
% CACH2 DRY .0
% CACO3 - DRY 5.0
% ASH DRY 1.0
% OTHER COMPOUNDS - DRY 7.0

** TREATMENT

METHOD BLEED
DEVICE N/A
PROPRIETARY PROCESS N/A

** DISPOSAL

NATURE FINAL
TYPE POND

LOCATION ON-SITE
SITE TRANSPORTATION METHOD PIPELINE
SITE TREATMENT CLAY LINING
SITE DIMENSIONS 34.8 ACRE X 25 FT
SITE SERVICE LIFE - YRS 20

ALABAMA ELECTRIC: TOMBIGBEE 2 (CONT.)

** PROCESS CONTROL AND INSTRUMENTATION CHEMICAL PARAMETERS

PHYSICAL VARIABLES PERCENT SOLIDS CONTROL LEVELS PH 5.8-6.0 MONITOR TYPE TBI MONITOR LOCATION RECYCLE TANK PROCESS CONTROL MANNER AUTOMATIC PROCESS CHEMISTRY MODE FEEDBACK

** WATER BALANCE

WATER LOOP TYPE CLOSED EVAPORATION WATER LOSS - LITER/S 10.5 (166 GPM) SLUDGE HYDRATION WATER LOSS - LITER/S 4 6PM)

POND SEEPAGE/RUNOFF WATER LOSS - LITERS/S 0

RECEIVING WATER STREAM TOMBIGBEE RIVER

MAKEUP WATER ADDITION - LITERS/S (157 GPM) 9.9 SOURCE OF MAKEUP WATER COOLING TOWER BLOWDOWN

** CHEMICALS AND CONSUMPTION

ABSORBENT FUNCTION NAME LIMESTONE PRINCIPAL CONSTITUENT 95% CACO3 SOURCE/SUPPLIER ALLIED PRODUCTS CO. CONSUMPTION 3.5 TPH [1.1 MOL/MOL SO2] UTILIZATION - % 90.0 POINT OF ADDITION BALL MILL

** FGD SPARE CAPACITY INDICES

ABSORBER - % . 0

** FGD SPARE COMPONENT INDICES

ABSORBER .0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS FACTOR

81.4 20.7 9/78 A 63.9 16.3 SYSTEM 18.5 720 183 133 81.4 72.7

** PROBLEMS/SOLUTIONS/COMMENTS

INITIAL OPERATION OF THE FGD SYSTEM BEGAN ON SEPTEMBER 23. THE SCRUBBER MODULES WERE FORCED OUT OF SERVICE 34 HOURS WHEN, AFTER CLOSING THE SYSTEM ISOLATION DAMPERS THE UTILITY WAS UNABLE TO OPEN THEM AGAIN.

342

45.7 10/78 A 57.0 В 57.7 46.2 SYSTEM 66.3 57.4 46.0 744 596

** PROBLEMS/SOLUTIONS/COMMENTS

BOILER SHUTDOWN.

ON OCTOBER 18 THE SUPERNATE LINE STARTED LEAKING. REPAIRS WERE MADE TO THE FIBERGLASS PIPING.

78.2 11/78 A 82.4 49.3 46.8 В SYSTEM 88.9 65.9 62.5 720 684 450

** PROBLEMS/SOLUTIONS/COMMENTS

IN LATE OCTOBER AND EARLY NOVEMBER A FIBERGLASS ELBOW IN THE WASTE SLURRY PIPE RUPTURED AND HAD TO BE REPLACED.

UTILITY FGD SURVEY: OCTOBER 1983 - SEPTEMBER 1984

ALABAMA ELECTRIC: TOMBIGBEE 2 (CONT.)

PERIOD	MODULE AV		PERF TY OPERABILITY RELIABI	LITY UTILIZATION	% REMO	VAL PART. 1	PER HOURS	BOILER HOURS	HOURS	CAP. FACTOR
			THE WASTE SLURRY AND ARCHITECT-ENGINEER.							
12/78	A		97.6	91.8						
	В		93.2	87.6						
	SYSTEM	97.8	95.4	89.7			744	700	668	
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			DOWNTIME DURING DECEM	BER WAS NOT ATTRI	BUTABLE	το π	HE FG	SYSTE	м.	
1/79	A		75 <i>.</i> 3	75.1						
	В		65.8	65.6						
	SYSTEM	89.2	70.6	70.4			744	742	524	
	** PROBLE	EMS/SOLUT	IONS/COMMENTS							
			SOME PLUGGING WAS END THE SYSTEM WAS DOWN F CLEANED.							
2/79	A		95.0	42.0						
	В		96.3	42.6						
	SYSTEM	98.4	95.7	42.3			672	297	284	
3/79	A		93.1	92. 2						
	В		94.4	93.6						
	SYSTEM	94.5	93.8	92.9			744	737	691	
4/79	A		100.0	40.6						
	В		100.0	40.6						
	SYSTEM	100.0	100.0	40.6			720	292	292	
	** PROBL	EMS/SOLUT	IONS/COMMENTS							
			THE UTILITY HAS REPOR	RTED THAT NO UNUSU	JAL PROE	LEMS I	HAVE (OCCURRE	D.	
5/79	A		48.8	47.6						
	В		58.9	57.4						
	SYSTEM	92.7	53.9	52.5			744	725	391	
6/79	A		1.8	1.0						
	В		95.4	51.8						
	SYSTEM	98.3	48.6	26.4			720	391	190	
	** PROBL	EMS/SOLUT	IONS/COMMENTS							
			THE UTILITY REPORTED WITH THE EXCEPTION OF THE MIST ELIMINATORS	DOWN TIME REQUIR	RED TO R	EPLAC	E THE	MIST E	LIMINA	JUNE TORS.
	Δ		21.0	16.5						
7/79			70.9							
7/79	R			55.9						
7/79	B System	ח דם								
7/79	B SYSTEM	93.0	46.0	36.2			744	587	270	
7/79 8/79	SYSTEM A	93.0	88.9	67.6			/44	507	270	
	SYSTEM	93.0					744	567	270	

THE SCRUBBER WAS NOT OPERATED FOR ABOUT 6 HOURS DUE TO A NECESSARY ADJUSTMENT TO THE MODICON CONTROLLER.

** PROBLEMS/SOLUTIONS/COMMENTS

PERIOD	MODULE AVAI	LABILI		PERFORMANCE DATA ABILITY UTILIZATION % REMOVA SO2 PAR	L PER BOI	LER FGD CAP
			THE SCRUBBER WAS E	SYPASSED FOR ABOUT 37 HOURS DU	E TO AN ESP	OUTAGE.
9/79	В	100.0	83.3 21.8 52.6	68.3 17.9 43.1	720 5	
			IONS/COMMENTS			
	AA TRODEETIS	, 30201				
			SEPTEMBER.	FED THAT THE SYSTEM WAS AVAILA	BLE AT ALL T	IMES DURING
10/79	SYSTEM	100.0		.0	744	0 0
	** PROBLEMS	/SOLUT	IONS/COMMENTS			
			THE UNIT NO. 2 GEN	NERATOR WAS DOWN THE ENTIRE MO	NTH OF OCTOB	SER.
11/79	SYSTEM	100.0		.0	720	0 0
	** PROBLEMS	/SOLUT	IONS/COMMENTS			
			THE GENERATOR REMA	AINED DOWN THROUGH NOVEMBER.		
12/79	A		22.6	4.0		
	B System	96.7	6.0 14.3	1.1 2.6	744 1	133 19
	** PROBLEMS	S/SOLUT	IONS/COMMENTS			
			THE OPERABILITY OF	THE FGD UNIT WAS LOW DUE TO	THE START-UF	OF THE BOILER
			THE FGD SYSTEM WAS	5 NOT AVAILABLE FOR 24 HOURS D	UE TO A RUPT	TURED WASTE
1/80	A		35.8	21.1		
	B System	90.7	56.7 46.3	33.5 27.3	744 4	39 203
			IONS/COMMENTS	2000		
	,		DURING JANUARY UN:	IT 2 WAS UNAVAILABLE 69 HOURS ION JOINT AND A RUPTURED WASTE		
2/80	A		84.3	84.3		
	B System	99.3	74.7 79.5	74.7 79.5	696 6	596 554
			IONS/COMMENTS		0,0	,,,
			THE UNIT 2 FGD SYS	BTEM OPERATED ALL BUT 5 HOURS AS BEING BROUGHT ON-LINE.	DURING FEBRU	JARY, IN WHICH
3/80	A		81.6	75.0		
	B System	100.0	79.4 80.5	73.0 74. 0	744 6	584 551
			IONS/COMMENTS	77.4	744	704 331
				BLEMS WERE ENCOUNTERED DURING THE TIME.	MARCH. THE	FGD SYSTEM WAS
4/80	A		61.3	61.3		
	В	100.0	86.6 74.0	86.5 73.9	720 '	710 F32
	SYSTEM	100.0	/7.0	/3.7	720	719 532

UTILITY FGD SURVEY: OCTOBER 1983 - SEPTEMBER 1984

ALABAMA ELECTRIC: TOMBIGBEE 2 (CONT.)

	MODULE AV	VAILABILI	TY OPERABILITY	RELIABILITY	UTILIZATION	% REMOVAL SO2 PART.	PER HOURS	BOILER HOURS	FGD HOURS	FACTOR
	** PROBLE	EMS/SOLUT	IONS/COMMENTS							
			THE UTILITY R			H OF APRIL	THE SY:	STEM WA	S	
5/80	A		34.9		34.7					
	B System	100.0	92. 8 6 3. 9		92.2 63.5		744	739	472	
			IONS/COMMENTS							
			THE FGD SYSTE	M WAS AVAILA	BLE 100% OF T	HE MONTH OF	MAY.			
6/80	A	100.0	88.0	100.0	11.0					
	B SYSTEM	.0 50.0	.0 44 0	.0 50.0	.0 5.5		720	90	40	7.0
			IONS/COMMENTS	20.0	3.3		720	7.5		
	W PROBL	21107 00201	MODULE B WAS DAMPER DRIVE		CE THE ENTIRE	MONTH OF J	UNE DU	E TO A	DAMAGEI	D
			MODULE A WAS ONLY 79 HOURS		R OPERATION T	HE ENTIRE M	ONTH, I	BUT WAS	NEEDE	D
7/80	A	100.0	97.6	100.0	54.5					
	B	.0		.0 50.0	.0		744	415	203	24 7
	SYSTEM			50.0	27.3		744	415	203	20.7
	** PROBL	EMS/SULUT	THE B-MODULE	PEMATNED OUT	OF SERVICE T	YIII HƏLIOQF	DUE T	n THE D	AMAGED	
			DAMPER DRIVE		or orkital i	JOE1	502 1		AAOLD	
			THE A-MODULE	OPERATED ON	AN AS NEEDED	BASIS WITH	NO PRO	BLEMS.		
		100.0		84.0						
8/80	B System	. 0 50.0		.0 42.0	.0 9.2		744	162	68	14.9
8/80										
8/80	** PROBL	EMS/SOLUT	IONS/COMMENTS							
8/80	** PROBL	EMS/SOLUT			MAINED OUT OF	SERVICE DU	E TO D	AMAGED	DAMPER	
9/80		EMS/SOLUT	DURING AUGUST OPERATOR MOTO		MAINED OUT OF	SERVICE DU	E TO D	AMAGED	DAMPER	
			DURING AUGUST OPERATOR MOTO	RS.		SERVICE DU	E TO D.			42.8

DURING SEPTEMBER MODULE B DID NOT OPERATE DUE TO A BURNED-UP DAMPER DRIVE MOTOR.

10/80	A	100.0	.0	.0				
	В	. 0	. 0	.0				
	SYSTEM	50.0	.0	.0	744	0	0	. 0

** PROBLEMS/SOLUTIONS/COMMENTS

DURING OCTOBER THE UNIT WAS OUT OF SERVICE FOR A TURBINE/GENERATOR INSPECTION.

PERIOD	MODULE AV	'AILABILI	TY OPERABILITY RE	LIABILITY	UTILIZATION				BOILER HOURS		CAP.
			REPAIR ON MODULE	B DAMPER	MOTOR DRIVE	CONTIN	UED T	THROUGH	OUT THE	монтн	
11/80	A	100.0	74.3	74.3	15.5						
	В	.0	.0	.0	0						
	SYSTEM	50.0	37.2	37.2	7.8			720	150	56	10.0
12/80	_	100.0		90.5	86.4						
	B System	62.4 81.2	62.9 76.7	62.9 76.7	60.1 73.2			744	710	545	45.9
	** PROBLE	MS/SOLUT	IONS/COMMENTS								
			MODULE B DAMPER REPORTED THAT NO QUARTER 1980.								JRTH
1/81	SYSTEM							744			
2/81	SYSTEM							672			
3/81	SYSTEM							744			
	** PROBLE	MS/SOLUT	IONS/COMMENTS								
			INFORMATION FOR	THE FIRST	QUARTER 198	L WAS N	VA TO	/AILABLI	E AT TH	IS TIM	Ε.
4/81	SYSTEM							720			
5/81	SYSTEM							744			
6/81	SYSTEM							720			
	** PROBLE	EMS/SOLUT	IONS/COMMENTS								
			INFORMATION FOR	THE SECON	D QUARTER 19	B1 WAS	NOT A	VAILAB	LE.		
7/81	SYSTEM							744			
	** PROBLE	MS/SOLUT	IONS/COMMENTS								
			INFORMATION FOR	THE MONTH	OF JULY WAS	NOT AV	'AILAE	SLE AT	THIS TI	ME.	
8/81		100.0	51.6	100.0	51.6						
	B	96.5	87.7	100.0	87.7			744	744	53.0	53 0
	SYSTEM	98.2	69.7	100.0	69.7			744	744	219	51.8
9/81	A	100.0	99.9	100.0	49.9						
	B System	95.1 97.6	95.2 70.9	100.0 100.0	92.0 70.9			720	720	511	6.2
			IONS/COMMENTS	100.0	, 0.,			720	720	211	0.2
	AA PRODE	1137 30 201	THE UTILITY REPO				ED PF	ROBLEMS	WERE E	NCOUNT	ERED
			DURING THE MONTH	IS UP AUGU	SI AND SEPTE	HBEK.					
10/01	A	16.9	3.5	3.5	.6						
10/81	D	16.9	99.6	99.6	16.8						
10/01	B System	16.9	51.5	51.5	8.7			744	125	65	4.0

THE UNIT AND THE FGD SYSTEM WERE OUT OF SERVICE FOR MOST OF OCTOBER FOR SCHEDULED MAINTENANCE.

ALABAMA ELECTRIC: TOMBIGBEE 2 (CONT.)

PERIOD	MODULE A		Y OPERABILIT		TY UTILIZATION	N % RE	10VAL	PER HOURS		FGD HOURS	CAP.
11/81	A	41.2	89.4								
	В	41.2	68.9	86 . 9	31.7						
	SYSTEM	41.2	79.1	88.2	36.4			720	331	262	22.9
	** PROBL	EMS/SOLUTI	DNS/COMMENTS								
			DURING NOVEM	BER THE SCH	EDULED MAINTE	NANCE S	TARTED	IN OC.	TOBER W	AS COM	PLETED.
12/81	A	100.0 100.0	97.1 10.7	100.0	96.8 10.7						
	В	100.0	10.7	100.0	10.7						
	SYSTEM	100.0	53.9	100.0	53.8			744	742	400	42.8
	** PROBL	.EMS/SOLUTI	ONS/COMMENTS								
			THE UTILITY DURING DECEM		T ROLAM ON TA	GD-RELA	TED PR	OBLEMS	WERE E	NCOUNT	ERED
1/82	A	93.3	93.4	93.4	93.4						
	SYSTEM	93.3	.6 45.5	47.1	45.5			744	744	350	46.8
	** PROBL	.EMS/SOLUTI	ONS/COMMENTS								
					STONE FEED SYSTEM		DZE CA	USING	AN UNAV	AILABI	LITY
2/82	Δ	100.0	98.3	100.0	81.5						
	B	100.0	.0		.0						
					40.7			672	557	274	38.2
	** PROBI	_EMS/SOLUTI	ONS/COMMENTS								
			DURING FEBRU	OLAM ON YSA	R FGD-RELATED	PROBLE	MS WER	E ENCO	UNTERED	•	
3/82	A	78.2	48.5	66.9	44.0						
	В	98.6	52.7	97.3	47.8						
	SYSTEM	88.4	50.6	82.1	47.8 45.9			744	675	342	38.4
	** PROBI	LEMS/SOLUTI	ONS/COMMENTS								
			DURING MARCH	THE MODULE	A HYDROCLONE	MALFUN	CTIONE	D CAUS	ING SOM	E OUTA	GE
4/82	Δ	84.3	74.2	82.5	74.0						
., 52	B	86.0	43.8	99.7	43.8						
	SYSTEM	85.1	59.0	91.1	58.9			720	718	424	54.0
5/82		100.0	04.0	700.0							
3/02	В		84.2	100.0	20.7						
	SYSTEM	100.0 100.0	93.7 88.9	100.0 100.0	23.0 21.9			744	183	163	14.2
		_EMS/SOLUTI	ONS/COMMENTS					, , ,	103	103	*
			NO MAJOR FGD	-RELATED PR	OBLEMS WERE R	EPORTED	DURIN	G THE	моитнѕ	OF APR	IL AND
6/82	SYSTEM	99.2	99.5	99.5	99.5			72 0	720	716	52.8
	** PROBI	EMS/SOLUTT	ONS/COMMENTS								
			THE UTILITY JUNE.	REPORTED EX	PERIENCING PR	OBLEMS	WITH T	HE 2A	OUTLET	DAMPER	DURING
7/82	SYSTEM	100.0	100.0	100.0	100.0			744	744	744	58.0

PERIOD	MODULE	AVAILABILIT	Y OPERABILITY	RELIABILITY		% REMOVAL SO2 PART.				
	** PROE	BLEMS/SOLUTIO	ONS/COMMENTS							
			THE UTILITY R	EPORTED THAT	NO MAJOR FGD	-RELATED PR	OBLEMS	WERE EI	NCOUNTI	ERED
8/82	SYSTEM	90.2	88.8	88.8	88.8		744	744	661	57.9
	** PRO	BLEMS/SOLUTIO	DNS/COMMENTS							
			THE UTILITY R		RIENCING PROE	BLEMS WITH T	HE 2A A	ND 2B (DAMPERS	5
9/82	SYSTEM	97.8	97.1	97.1	97.8		720	664	704	48.0
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
			THE 2A DAMPER	S WERE OUT O	F SERVICE DUR	ING PART OF	SEPTEM	BER FO	R REPA	IRS.
			THE SCRUBBER	-		DURING PART	OF SEF	TEMBER	WHILE	THE
10/82	SYSTEM	.0			.0		744	0	0	.0
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS							
			THE UTILITY R	EPORTED THAT	THE BOILER	NAS SHUT DOW	N DURIN	1G OCTO	BER.	
11/82	SYSTEM	74.7	98.4	98.4	73.9		720	540	532	49.1
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS							
			A BROKEN DAMP	ER CHAIN RES	ULTED IN DOWN	N TIME DURIN	G NOVE	1BER.		
12/82	SYSTEM	95.2	95.0	95.0	90.8		744	711	676	48.2
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS							
			THE UTILITY R DURING DECEMB		NO MAJOR FG	-RELATED PR	OBLEMS	WERE E	NCOUNT	ERED
1/83	SYSTEM	100.0	100.0	100.0	100.0		744	744	744	59.2
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS							
			-NO MAJOR FGD NANNAR BNIRUD		LEMS WERE EN	COUNTERED BY	THE U	TILITY		
2/83	SYSTEM	100.0	99.4	99.4	93.2		672	630	62 6	66.5
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS							
			THE UTILITY R	EPORTED THAT	THE UNIT WAS	S SHUT DOWN	DURING	PART O	F FEBR	UARY.
3/83	SYSTEM	100.0	100.0	100.0	100.0		744	744	744	74.6
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS							
			NO MAJOR FGD- DURING MARCH.	RELATED PROB	LEMS WERE EN	COUNTERED BY	THE U	TILITY		
	AVATE::									

98.1

82.0

.0

720 602

0

744

591 60.6

0

89.7 98.1

4/83 SYSTEM

5/83 SYSTEM

ALABAMA ELECTRIC: TOMBIGBEE 2 (CONT.)

ERIOD			Y OPERABILITY			SO2 PART.	HOURS	BOILER HOURS	FGD HOURS	FACTOR
6/83	SYSTEM				.0		720	0	0	
	** PROBLE	MS/SOLUTI	ONS/COMMENTS							
			THE UTILITY R			IAS SHUT DOW	N DURI	NG MAY	AND JUI	NE FOR
7/83	A	83.9	73.6		62.9					
	B SYSTEM	83.9 83.9			19.4 41.1		744	637	306	51.3
					41.1					5215
	** PROBLE	EMS/SOLUTI	ONS/COMMENTS							
			THE UTILITY F DURING JULY.	REPORTED THAT	NO MAJOR FGD	-RELATED PR	OBLEMS	WERE E	NCOUNT	ERED
8/83	A	96.9	78.3		78.2					
	B SYSTEM	100.0 98.5	-		21.7 49.9		744	743	372	65.8
			-		77.7		, , , ,	7.5	372	03.0
	** PROBLI	EMS/SOLUT	ONS/COMMENTS							
			MODULE A WAS ANCE.	OUT OF SERVI	CE DURING PAR	T OF AUGUST	FOR P	RESATUR	ATOR M	AINTEN
9/83	A		25.7		25.4					
	B SYSTEM	100.0 100.0	73.8 49.8		73.1 49.3		72 0	712	355	51.9
	** PROBL	EMS/SOLUT	IONS/COMMENTS							
			THE UTILITY I	REPORTED THAT MBER.	NO MAJOR FGE	-RELATED PR	OBLEMS	WERE E	NCOUNT	ERED
10/83	A	81.5			10.8					
	B System	81.5 81.5	97.4 55.2	55.2	80.5 45.6		7/./	615	740	53.3
					45.0		/44	013	340	23.3
	** FROBL	EMS/SOLUT	ICNS/COMMENTS							
			NO MAJOR FGD	-RELATED PROB	LEMS WERE REF	PORTED DURIN	G OCTO	BER.		
11/83	SYSTEM				.0		720	0	0	.0
	** PROBL	EMS/SOLUT	IONS/COMMENTS							
			THE UNIT WAS	OFF LINE DUR	ING NOVEMBER	FOR A SCHED	ULED F	ALL OUT	AGE.	
12/83		.0	.0		. 0					
	B System	.0	.0 .0	. 0	.0		7//	340	•	
					.0		744	149	0	9.9
	** FRUBL	EMS/SOLUT	IONS/COMMENTS							
			DECEMBER. P	WEATHER COND IPING ASSOCIA ROZEN, PLUGGE	TED WITH LIM	ESTONE SLURR	STEM O	UT OF S	ERVICE AGENT	DURIN PREPA-
1/84	A	45.4	18.8		18.8					
	₿	80.0	62.5		62.5					
	SYSTEM	62.7	40.6	40.6	40.6		744	744		55.2

	MODULE A	VAILABILI	TY OPERABILIT	Y RELIABILITY	Y UTILIZATION	% REMOVAL SO2 PART.		BOILER HOURS	FGD HOURS	CAP.
	** PROBL	EMS/SOLUT	IONS/COMMENTS	3						
			THE UTILITY	REPORTED THAT	THE ABSORBER	WAS INOPERA	ABLE DU	JE TO F	ROZEN F	PIPES.
			THE UTILITY	REPORTED LIME	ESTONE FEED AN	TO BALL MILL	PROBLE	MS DUR	ING JAN	WARY.
2/84	В	100.0	81.4 90.5 85.9	25.0	81.4 90.5				500	62.4
	SYSTEM	100.0		85.9	85.9		696	696	570	62.4
	** PROBL	EMS/SOLUT	IONS/COMMENTS	5						
			THE UTILITY DURING FEBRU		T NO MAJOR FGD	-RELATED PRO	BLEMS	WERE EI	NCOUNTE	RED
3/84	A	31.9			30.2					
	B System	31.9 31.9	84.7 85.1	30.1	29.9 30.1		744	263	224	25.1
			IONS/COMMENTS	-	3412				'	
	** PRODL	E1137 30 LUT								_
			STACK.	WAS REMOVED	FROM SERVICE	DURING MARCH	то не	LP DRY	OUT TH	IE
			THE UTILITY	REPORTED THAT	T A UNIT TURBI	INE OUTAGE IN	NSPECT1	TON OCC	JRRED.	
4/84		.0	THE UTILITY		.0	INE OUTAGE IN	NSPECT]	ION OCCI	URRED.	
4/84	A B System	.0 .0	THE UTILITY	REPORTED THAT	_	NE OUTAGE IN	15PECT] 720	0 000	URRED.	.0
4/84	B SYSTEM	.0	THE UTILITY		. 0 . 0	NE O UTAGE IN				.0
4/84	B SYSTEM	.0	IONS/COMMENTS		. 0 . 0		720	0		.0
	B SYSTEM ** PROBL	.0	IONS/COMMENTS		0. 0. 0.		720	0		.0
	B SYSTEM ** PROBL A B	.0 .0 EMS/SOLUT 12.9 12.9	IONS/COMMENTS THE UTILITY 3.4 54.3	REPORTED A U	.0 .0 .0 MIT SHUT DOWN .8 12.2		720 RBINE (O DUTAGE.	0	
	B SYSTEM ** PROBL	.0 .0 EMS/SOLUT 12.9	IONS/COMMENTS THE UTILITY 3.4		.0 .0 .0 MIT SHUT DOWN .8 12.2		720	O DUTAGE.	0	.0
4/84 5/84	B SYSTEM ** PROBL A B SYSTEM	.0 .0 EMS/SOLUT 12.9 12.9 12.9	IONS/COMMENTS THE UTILITY 3.4 54.3	. REPORTED A UM 6.5	.0 .0 .0 MIT SHUT DOWN .8 12.2		720 RBINE (O DUTAGE.	0	
	B SYSTEM ** PROBL A B SYSTEM	.0 .0 EMS/SOLUT 12.9 12.9 12.9	IONS/COMMENTS THE UTILITY 3.4 54.3 28.8 IONS/COMMENTS	. REPORTED A UT 6.5	.0 .0 .0 MIT SHUT DOWN .8 12.2	DUE TO A TUT	720 RBINE (0 DUTAGE. 167	0	10.4
5/84	B SYSTEM ** PROBL A B SYSTEM	.0 .0 EMS/SOLUT 12.9 12.9 12.9	IONS/COMMENTS THE UTILITY 3.4 54.3 28.8 IONS/COMMENTS	. REPORTED A UT 6.5	.0 .0 .0 NIT SHUT DOWN .8 12.2 6.5	DUE TO A TUT	720 RBINE (0 DUTAGE. 167	0	10.4
5/84	B SYSTEM ** PROBL A B SYSTEM ** PROBL A B	.0 .0 EMS/SOLUT 12.9 12.9 12.9 EMS/SOLUT	IONS/COMMENTS THE UTILITY 3.4 54.3 28.8 IONS/COMMENTS THE ABSORBER THE STACK. 77.0 53.7	. REPORTED A UN 6.5 R WAS DOWN SET	.0 .0 .0 NIT SHUT DOWN .8 12.2 6.5 VERAL DAYS DUF 77.0 53.7	DUE TO A TUT	720 RBINE (744 ALLOW H	O DUTAGE. 167 HOT FLU	0 48 E GAS 1	10.4 TO DRY
5/84	B SYSTEM ** PROBL A B SYSTEM ** PROBL A B SYSTEM	.0 .0 EMS/SOLUT 12.9 12.9 12.9 EMS/SOLUT	IONS/COMMENTS THE UTILITY 3.4 54.3 28.8 IONS/COMMENTS THE ABSORBER THE STACK. 77.0 53.7 65.3	REPORTED A UN 6.5 R WAS DOWN SET	.0 .0 .0 NIT SHUT DOWN .8 12.2 6.5 VERAL DAYS DUR	DUE TO A TUT	720 RBINE (O DUTAGE. 167 HOT FLU	0	10.4 TO DRY
5/84	B SYSTEM ** PROBL A B SYSTEM ** PROBL A B SYSTEM	.0 .0 EMS/SOLUT 12.9 12.9 12.9 EMS/SOLUT	IONS/COMMENTS THE UTILITY 3.4 54.3 28.8 IONS/COMMENTS THE ABSORBER THE STACK. 77.0 53.7	REPORTED A UN 6.5 R WAS DOWN SET	.0 .0 .0 NIT SHUT DOWN .8 12.2 6.5 VERAL DAYS DUF 77.0 53.7	DUE TO A TUT	720 RBINE (744 ALLOW H	O DUTAGE. 167 HOT FLU	0 48 E GAS 1	10.4 TO DRY
5/84	B SYSTEM ** PROBL A B SYSTEM ** PROBL A B SYSTEM	.0 .0 EMS/SOLUT 12.9 12.9 12.9 EMS/SOLUT	IONS/COMMENTS THE UTILITY 3.4 54.3 28.8 IONS/COMMENTS THE ABSORBEE THE STACK. 77.0 53.7 65.3 IONS/COMMENTS	REPORTED A UN 6.5 R WAS DOWN SET 65.3 REPORTED THA	.0 .0 .0 NIT SHUT DOWN .8 12.2 6.5 VERAL DAYS DUF 77.0 53.7	DUE TO A TUT	720 RBINE 0 744 ALLOW H	O DUTAGE. 167 HOT FLU 720	0 48 E GAS 1 470	10.4 FO DRY 61.2

** PROBLEMS/SOLUTIONS/COMMENTS

8/84 SYSTEM

9/84 SYSTEM

INFORMATION WAS UNAVAILABLE FOR THE THIRD QUARTER OF 1984.

744

720

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COMPANY NAME ALABAMA ELECTRIC TOMBIGBEE PLANT NAME UNIT NUMBER LEROY CITY ALABAMA STATE 43. (.100 LB/MMBTU)
516. (1.200 LB/MMBTU)
301. (.700 LB/MMBTU)
525
255
235 REGULATORY CLASSIFICATION PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW 525
GROSS UNIT GENERATING CAPACITY MW 255
NET UNIT GENERATING CAPACITY W/FGD - MW 235
NET UNIT GENERATING CAPACITY W0/FGD - MW 243 EQUIVALENT SCRUBBED CAPACITY MW 179 ** UNIT DATA - BOILER AND STACK RILEY STOKER BOILER SUPPLIER BOILER SUPPLIER

BOILER TYPE

BOILER SERVICE LOAD

DESIGN BOILER FLUE GAS FLOW - CU.M/S

BOILER FLUE GAS TEMPERATURE - C

STACK HEIGHT M

STACK SHELL

STACK TOP DIAMETER - M

RILET STUKER
PULVERIZED COAL

BASE

1449.72 (953000 ACFM)

143.9 (291 F)

122. (400 FT)

CONCRETE

5.0 (16.5 FT) ** FUEL DATA FUEL TYPE BITUMINOUS FUEL GRADE 26572. AVERAGE HEAT CONTENT - J/G (11424 BTU/LB) RANGE HEAT CONTENT - BTU/LB AVERAGE ASH CONTENT - % 10000-11000 14.73 15-18 6.64 3.0-20.0 1.61 RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - %
RANGE MOISTURE CONTENT %
AVERAGE SULFUR CONTENT %
RANGE SULFUR CONTENT - %
AVERAGE CHLORIDE CONTENT %
RANGE CHLORIDE CONTENT % AVERAGE MOISTURE CONTENT - % 6.64 3.0-20.0 1.5-1.75 .04 ***** 1.61 RANGE CHLORIDE CONTENT % *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER TYPE NONE ** ESP NUMBER NUMBER OF SPARES D HOT SIDE TYPF SUPPLIER

RESEARCH-COTTRELL

INLET FLUE GAS CAPACITY CU.M/S 449.7 (953000 ACFM)

INLET FLUE GAS TEMPERATURE C 143.9 (291 F)

PRESSURE DROP - KPA .1 (1. IN-H20)

PARTICLE REMOVAL EFFICENCY - % 99.5 ** PARTICLE SCRUBBER NUMBER GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL N/A LINER GENERIC MATERIAL N/A LINER SPECIFIC MATERIAL N/A GAS CONTACTING DEVICE TYPE N/A

*** FGD SYSTEM

ALABAMA ELECTRIC: TOMBIGBEE 3 (CONT.)

```
** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                             THROWAWAY PRODUCT
                                             WET SCRUBBING
   SO2 REMOVAL MODE
   PROCESS TYPE
                                              LIMESTONE
   PROCESS ADDITIVES
                                              NONE
   SYSTEM SUPPLIER
                                              PEABODY PROCESS SYSTEMS
   A-E FIRM
                                              BURNS & MCDONNELL
   DEVELOPMENT LEVEL
                                              FULL SCALE
   NEW/RETROFIT
                                              NEW
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.50
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                59.50
    ENERGY CONSUMPTION - %
                                                 3.1
   CURRENT STATUS
    COMMERCIAL START-UP
                                               6/79
    INITIAL START-UP
                                               6/79
   CONTRACT AWARDED
                                               8/75
** DESIGN AND OPERATING PARAMETERS
                                                1.48
   DESIGN COAL SULFER CONTENT - %
    DESIGN COAL HEAT CONTENT - J/G
                                              29075.0
                                                             ( 12500 BTU/LB)
                                               10.00
    DESIGN COAL ASH CONTENT - %
                                                8.00
    DESIGN MOISTURE CONTENT - %
    DESIGN CHLORIDE CONTENT - %
                                                   .04
                                              4645.0
    SPACE REQUIREMENTS - SQ M
                                                           ( 50000 SQ FT)
    OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                72.0
** QUENCHER/PRESATURATOR
   NUMBER
    TYPE
                                              SPRAY
                                              127.41 ( 270000 ACFM)
143.9 ( 291 F)
35. ( 550 GPM)
    INLET GAS FLOW - CU. M/S
                                                            ( 291 F)
( 550 GPM)
    INLET GAS TEMPERATURE - C
    LIGUID RECIRCULATION RATE - LITERS/S
                                                35.
    CONSTRUCTION MATERIAL GENERIC TYPE
                                            HIGH ALLOY
                                            NICKEL BASE/CHROMIUM-IRON-COPPER-MOLYBDENUM
    CONSTRUCTION MATERIAL SPECIFIC TYPE
** ABSORBER
    NUMBER
                                               2
    NUMBER OF SPARES
                                               n
    GENERIC TYPE
                                              SPRAY TOWER
                                              OPEN COUNTERCURRENT SPRAY
    SPECIFIC TYPE
    TRADE NAME/COMMON TYPE
                                              N/A
    SUPPLIER
                                              PEABODY PROCESS SYSTEMS
    DIMENSIONS - FT
                                              24.0 DIA X 90.0
    SHELL GENERIC MATERIAL
                                              CARBON STEEL
    SHELL SPECIFIC MATERIAL
                                              AISI 1110
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                            N/A
    LINER GENERIC MATERIAL
                                              ORGANIC
    LINER SPECIFIC MATERIAL
                                              GLASS FLAKE-FILLED POLYESTER
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                             RESISTA-FLAKE 1151
    GAS CONTACTING DEVICE TYPE
                                             NONE
    NUMBER OF CONTACTING ZONES
                                              6
    LIQUID RECIRCULATION RATE - LITER/S
                                              1259.
                                                           (19980 GPM)
                                               9.9
                                                           ( 74.0 GAL/1000 ACF)
    L/G RATIO - L/CU.M
    GAS-SIDE PRESSURE DROP - KPA
                                                 1.0
                                                            ( 4.0 IN-H20)
    SUPERFICAL GAS VELOCITY M/SEC
                                                  3.0
                                                           ( 10.0 FT/S)
    INLET GAS FLOW - CU. M/S
                                               127.41
                                                            ( 270000 ACFM)
                                                            ( 130 F)
    INLET GAS TEMPERATURE - C
                                                54.4
    SO2 REMOVAL EFFICIENCY - %
                                                85.0
                                                 99 5
    PARTICLE REMOVAL EFFICENCY - %
** MIST ELIMINATOR
                                            PRIMARY COLLECTOR
    PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                              2
    NUMBER PER SYSTEM
    NUMBER OF SPARES PER SYSTEM
                                               0
    NUMBER PER MODULE
                                               1
                                              IMPINGEMENT
    GENERIC TYPE
    SPECIFIC TYPE
                                              BAFFLE
    TRADE NAME/COMMON TYPE
                                              CLOSED VANE
                                              SHAH-HEIL
    MANUFACTURER
                                              HORIZONTAL
    CONFIGURATION
```

ALABAMA ELECTRIC: TOMBIGBEE 3 (CONT.)

```
NUMBER OF STAGES
                                                  1
   NUMBER OF PASSES PER STAGE
                                                  1
   FREEBOARD DISTANCE M
                                                  1.22
                                                            ( 4.0 FT)
                                                   .1
   PRESSURE DROP - KPA
                                                             ( .5 IN-H20)
   SUPERFICAL GAS VELOCITY - M/S
                                                  3.0
                                                             ( 10.0 FT/S)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              ORGANIC
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              POLYPHENYLENE
                                              MAKEUP
   WASH WATER SOURCE
                                              INTERMITTENTLY
   WASH FREQUENCY
** DEHEATED
   NUMBER
                                               1
                                              BYPASS
   GENERIC TYPE
    SPECIFIC TYPE
                                              COLD SIDE
   TRADE NAME/COMMON TYPE
                                              N/A
                                              ABSORBER OUTLET DUCT
    LOCATION
                                                30.0
    PERCENT GAS BYPASSED - AVG
                                                             ( 48 F)
    TEMPERATURE INCREASE - C
                                                 26.7
   INLET FLUE GAS FLOW RATE - CU. M/S
                                               134.92
                                                            ( 285900 ACFM)
                                                             ( 291 F)
( 178 F)
    INLET FLUE GAS TEMPERATURE - C
                                               143.9
    OUTLET FLUE GAS TEMPERATURE - C
                                                 81.1
    CONSTRUCTION MATERIAL GENERIC TYPE
                                             HIGH ALLOY
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                             NICKEL BASE/CHROMIUM-IRON-MOLYBDENUM
** FANS
                                               2
   NUMBER
    NUMBER OF SPARES
                                               0
                                              CENTRIFUGAL
    DESIGN
                                              PEABODY PROCESS SYSTEMS
    SUPPLIER
    FUNCTION
                                              UNTT
    APPLICATION
                                              FORCED DRAFT
    SERVICE
                                              DRY
    FLUE GAS FLOW RATE - CU.M/S
                                                225.10
                                                             ( 477000 ACFM)
    FLUE GAS TEMPERATURE - C
                                                143.9
                                                             ( 291 F)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                             CARBON STEEL
** DAMPERS
    NUMBER
                                               2
    FUNCTION
                                               SHUT-OFF
    GENERIC TYPE
                                              GUTLLOTINE
    MANUFACTURER
                                              MOSSER
    CONSTRUCTION MATERIAL GENERIC TYPE
                                              CARBON STEEL
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              NR
    LINER GENERIC MATERIAL TYPE
                                              HIGH ALLOY
    LINER SPECIFIC MATERIAL TYPE
                                              NICKEL BASE/CHROMIUM-IRON-COPPER-MOLYBDENUM
** DAMPERS
    NUMBER
                                               2
    FUNCTION
                                               SHUT-OFF
    GENERIC TYPE
                                              GUILLOTINE
    MANUFACTURER
                                              MOSSER
    CONSTRUCTION MATERIAL GENERIC TYPE
                                              CARBON STEFL
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              NΡ
    LINER GENERIC MATERIAL TYPE
                                              HIGH ALLOY
    LINER SPECIFIC MATERIAL TYPE
                                              NICKEL BASE/CHROMIUM-IRON-COPPER-MOLYBDENUM
** DAMPERS
    NUMBER
                                               2
    FUNCTION
                                              CONTROL
    GENERIC TYPE
                                               LOUVER
    MANUFACTURER
                                              MOSSER
    CONSTRUCTION MATERIAL GENERIC TYPE
                                              CARBON STEEL
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              NR
    LINER GENERIC MATERIAL TYPE
                                              NONE
    LINER SPECIFIC MATERIAL TYPE
                                              N/A
** DUCTWORK
    LOCATION
                                              SCRUBBER INLET
    CONFIGURATION
                                              RECTANGULAR
   DIMENSIONS
                                              7 FT X 12 FT
     SHELL GENERIC MATERIAL TYPE
                                              CARBON STEEL
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ALABAMA ELECTRIC: TOMBIGBEE 3 (CONT.)
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SHELL SPECIFIC MATERIAL TYPE AISI 1110 LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A

** DUCTWORK

LOCATION SCRUBBER OUTLET TO STACK CONFIGURATION RECTANGULAR DIMENSIONS 5.5 FT X 12 FT AND 13 FT X 16 FT SHELL GENERIC MATERIAL TYPE CARBON STEEL SHELL SPECIFIC MATERIAL TYPE AISI 1110 LINER GENERIC MATERIAL TYPE

ORGANIC LINER SPECIFIC MATERIAL TYPE FLUOROELASTOMER

** REAGENT PREPARATION EQUIPMENT

FUNCTION WET BALL MILL DEVICE COMPARTMENTED DEVICE TYPE NR MANUFACTURER KENNEDY VAN SAUN NUMBER

FULL LOAD DRY FEED CAPACITY - M.TONS/HR 9.1 (10 TPH) PRODUCT QUALITY ~ % SOLIDS 35.0

** TANKS

SERVICE NUMBER ABSORBER RECYCLE 1 MIST ELIMINATOR WASH LIMESTONE SLURRY STORAGE 1 HYDROCLONE UNDERFLOW *** MILL RECYCLE SUMP 1 WASTE SLURRY SUMP 1

** PUMPS

NUMBER SERVICE ABSORBER RECIRCULATION 6 LIMESTONE MILL SLURRY RECIRCULATION 2 LIMESTONE SLURRY FEED 2 MIST ELIMINATOR WASH 3 WASTE SLURRY 2 SUPERNATE RETURN 1

** SOLIDS CONCENTRATING/DEWATERING

DEVICE NONE

*** SLUDGE

FULL LOAD SLUDGE QUANTITY - M.TONS/HR (DRY) 5.6 6.2 TPH) % CASO3 - DRY 17.0 % CASO4 - DRY 70.0 % CAOH2 - DRY . 0 5.0 % CACO3 - DRY % ASH - DRY 1.0 % OTHER COMPOUNDS - DRY 7.0

** TREATMENT

BLEED METHOD DEVICE N/A PROPRIETARY PROCESS N/A

** DISPOSAL

NATURE FINAL TYPE POND LOCATION ON-SITE PIPELINE SITE TRANSPORTATION METHOD SITE TREATMENT CLAY LINING SITE DIMENSIONS 34.8 ACRE X 25 FT

SITE SERVICE LIFE - YRS 20 UTILITY FGD SURVEY: OCTOBER 1983 - SEPTEMBER 1984

ALABAMA ELECTRIC: TOMBIGBEE 3 (CONT.)

** PROCESS CONTROL AND INSTRUMENTATION

CHEMICAL PARAMETERS PΗ PERCENT SOLIDS PHYSICAL VARIABLES PH 5.8-6.0 CONTROL LEVELS TRT MONITOR TYPE RECYCLE TANK MONITOR LOCATION AUTOMATIC PROCESS CONTROL MANNER PROCESS CHEMISTRY MODE FEEDBACK

** WATER BALANCE

CLOSED WATER LOOP TYPE (166 GPM) EVAPORATION WATER LOSS - LITER/S 10.5 (4 GPM) SLUDGE HYDRATION WATER LOSS - LITER/S . 3 POND SEEPAGE/RUNOFF WATER LOSS - LITERS/S 0 TOMBIGBEE RIVER RECEIVING WATER STREAM

9.9 MAKEUP WATER ADDITION - LITERS/S

(157 GPM) COOLING TOWER BLOWDOWN SOURCE OF MAKEUP WATER

** CHEMICALS AND CONSUMPTION

ABSORBENT FUNCTION LIMESTONE NAME 95% CACO3 PRINCIPAL CONSTITUENT ALLIED PRODUCTS CO. SOURCE/SUPPLIER CONSUMPTION 3.5 TPH [1.1 MOL/MOL SO2] 90.0 UTILIZATION - % BALL MILL POINT OF ADDITION

** FGD SPARE CAPACITY INDICES

ABSORBER - % .0

** FGD SPARE COMPONENT INDICES . 0 ABSORBER

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

7/79 A 23.7 9.4 В 27.8 11.0 SYSTEM 72.7 25.8 10.2 744 295 76

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM IS CURRENTLY UNDERGOING SHAKEDOWN/DEBUGGING OPERATIONS.

8/79 A 59.4 39.1 В 44.5 29.3 SYSTEM 99.7 52.0 34.2 744 490 255

** PROBLEMS/SOLUTIONS/COMMENTS

AN ADJUSTMENT TO THE MODICON CONTROLLER CAUSED A SCRUBBER OUTAGE OF ABOUT TWO HOURS.

THE SCRUBBER WAS DOWN DURING AN ESP OUTAGE FOR APPROXIMATELY 34 HOURS.

9/79 A 73.0 13.9 11.0 2.1 SYSTEM 100.0 42.0 72**0** 137 58 8.0

** PROBLEMS/SOLUTIONS/COMMENTS

CONTINUING GENERATOR PROBLEMS RESULTED IN LOW FGD SYSTEM UTILIZATION DURING SEPTEMBER.

10/79 A 82.7 82.7

ERIOD	MODULE AVA		TY OPERABILITY RELIAE		% REI	10VAL PART.	PER HOURS	HOURS	HOURS	CAP.
	В		90.9	90.9						
	SYSTEM	99.5	86.8	86.8			744	744	646	
	** PROBLEM	15/50LUT	IONS/COMMENTS							
			THE FGD SYSTEM WAS SESP TESTS.	SHUT DOWN FOR 37 HO	URS FO	OR BOI	LER STA	ART-UPS	AND	
			PROBLEMS WITH THE LI A SHORTAGE OF REAGEN							
1/79	A		78.6	78.6						
	В	a	89.3	89.3			700	700		
	SYSTEM	96.7	84.0	84.0			720	720	605	
	** PROBLE	15/50LUT	IONS/COMMENTS							
			DURING NOVEMBER THE HANDLING SYSTEM JAMP				CAUSE 1	THE ESP	FLYASH	l
			THE WASTE SLURRY LIN 24 HOURS.	E RUPTURED, FORCIN	G THE	UNIT	OUT OF	SERVIC	E FOR	
2/79	A		78.4	68.7						
	В		87.6	76.8						
	SYSTEM	100.0	83.0	72.8			744	652	541	
	** PROBLE	4S/SOLUT	IONS/COMMENTS							
			NO FGD SYSTEM PROBLE WAS AVAILABLE FOR TH		ם סעד:	ING DE	CEMBER.	. THE	FGD SYS	STEM
1/80	A		69.2	30.5						
	В		45.4	20.0						
	SYSTEM	100.0	57.3	25.3			744	328	188	
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			DURING JANUARY UNIT	3 WAS AVAILABLE TH	E ENT	IRE MO	NTH.			
2/80	A		33.3	1.2						
	В		100.0	3.5						
	SYSTEM	100.0	66.7	2.4			696	24	16	
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			DURING FEBRUARY THE THE FGD SYSTEM WAS				OPERATI	ED ONLY	24 HOU	JRS.
3/80	SYSTEM	100.0		.0			744	0	0	. 0
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			DURING MARCH THE UNI		KEPT	OUT OF	SERVI	CE. TH	E FGD S	SYSTEM
4/80	SYSTEM			.0			720	0	0	. 0
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			THE UTILITY REPORTED	THAT DURING APPTI	THE	BOILFR	יא מום	OT OPER	ATE.	
						COLLER	. 515 11	., J. L.R	~	
5/80	A		8.3	.7						

ALABAMA ELECTRIC: TOMBIGBEE 3 (CONT.)

12/80 A 100.0 B 100.0

SYSTEM

100.0

100.0

	HODOLE	AVAILABILITY	Y OPERABILITY	RELIABILITY	UTILIZATION	% REMOVAL SO2 PART.	PER HOURS	BOILER HOURS	FGD HOURS	CAP.
	B SYSTEM	95.8	.0 4.2		.0		744	60	5	
	** PROS	BLEMS/SOLUTIO	ONS/COMMENTS							
			THE FGD SYSTEM					VER, TH	E BOIL	R ONL
			THE B MODULE P			THE INLET	DAMPER	SWITCH	FAILE)
6/80	A	100.0	59.1	100.0	52.8					
	B	100.0	58.6	100.0	52.4					
	SYSTEM	100.0	58.9	100.0	52.6		720	643	379	52.0
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
		1	NO FGD SYSTEM-	RELATED PROE	LEMS WERE EN	COUNTERED D	URING .	JUNE.		
7/80	A	100.0	45.5	100.0	39.7					
	A B	100.0	90.0	100.0 100.0	78.6					
	SYSTEM	100.0	67.8	100.0	59.2		744	650	440	47.8
	** PRO	BLEMS/SOLUTION	ONS/COMMENTS							
			THE FGD SYSTEM MODULES ARE UT				TIRE M	ONTH OF	JULY.	THE
8/80	A		95.7	100.0	75.8					
8/80	A B	100.0	95.7 91.6	100.0 100.0	75.8 72.6					
8/80	A B SYSTEM	100.0	91.6	100.0 100.0 100.0	75.8 72.6 74.2		744	590	5 52	63.4
8/80	B SYSTEM	100.0 100.0 100.0	91.6	100.0	72.6		744	590	5 52	63.4
8/80	B SYSTEM	. 100.0 100.0 100.0	91.6 93.7	100.0	72.6 74.2	ED DURING T				63.4
8/80 9/80	B SYSTEM ** PRO	. 100.0 100.0 100.0 BLEMS/SOLUTION	91.6 93.7 ONS/COMMENTS NO FGD-RELATED	100.0 100.0 PROBLEMS WE	72.6 74.2 ERE ENCOUNTER 46.8	ED DURING T				63.4
	B SYSTEM ** PROD A B	. 100.0 100.0 100.0 BLEMS/SOLUTION	91.6 93.7 ONS/COMMENTS NO FGD-RELATED 91.4 73.7	100.0 100.0 PROBLEMS WE 91.4 73.7	72.6 74.2 ERE ENCOUNTER 46.8	ED DURING T				63.4
	B SYSTEM ** PRO	. 100.0 100.0 100.0 BLEMS/SOLUTION	91.6 93.7 ONS/COMMENTS NO FGD-RELATED 91.4 73.7	100.0 100.0 PROBLEMS WE	72.6 74.2 ERE ENCOUNTER 46.8	ED DURING T	HE MON		UGUST.	
9/80	B SYSTEM ** PROP	. 100.0 100.0 100.0 BLEMS/SOLUTION	91.6 93.7 DNS/COMMENTS NO FGD-RELATED 91.4 73.7 82.4	100.0 100.0 PROBLEMS WE 91.4 73.7 82.4 68.4	72.6 74.2 ERE ENCOUNTER 46.8 37.8 42.2 68.4	ED DURING T	HE MON	TH OF A	UGUST.	
9/80	B SYSTEM ** PROI A B SYSTEM A B	90.6 90.6 97.4 97.4	91.6 93.7 DNS/COMMENTS NO FGD-RELATED 91.4 73.7 82.4 68.4	100.0 100.0 PROBLEMS WE 91.4 73.7 82.4	72.6 74.2 ERE ENCOUNTER 46.8 37.8 42.2 68.4	ED DURING T	HE MON	TH OF A	UGUST.	
9/80	B SYSTEM ** PROI A B SYSTEM A	90.6 90.6 97.4 97.4	91.6 93.7 DNS/COMMENTS NO FGD-RELATED 91.4 73.7 82.4 68.4	100.0 100.0 PROBLEMS WE 91.4 73.7 82.4 68.4	72.6 74.2 ERE ENCOUNTER 46.8 37.8 42.2 68.4	ED DURING T	HE MON' 720	TH OF A	UGUST. 304	
	A B SYSTEM A B SYSTEM A B SYSTEM A	90.6 90.6 97.4 97.4 99.3	91.6 93.7 DNS/COMMENTS NO FGD-RELATED 91.4 73.7 82.4 68.4 60.9	100.0 100.0 PROBLEMS WE 91.4 73.7 82.4 68.4 60.9	72.6 74.2 ERE ENCOUNTER 46.8 37.8 42.2 68.4 60.9	ED DURING T	HE MON' 720	TH OF A	UGUST. 304	32.4
9/80 10/80	A B SYSTEM A B SYSTEM A B SYSTEM A B	90.6 90.6 97.4 97.4 97.4 99.3	91.6 93.7 ONS/COMMENTS NO FGD-RELATED 91.4 73.7 82.4 68.4 60.9 63.4 83.6 87.9	100.0 100.0 PROBLEMS WE 91.4 73.7 82.4 68.4 60.9 63.4 83.6 87.9	72.6 74.2 ERE ENCOUNTER 46.8 37.8 42.2 68.4 60.9 63.4	ED DURING T	HE MON' 720	TH OF A	UGUST. 304	32.4
9/80 10/80	A B SYSTEM A B SYSTEM A B SYSTEM A	90.6 90.6 97.4 97.4 97.4 99.3	91.6 93.7 ONS/COMMENTS NO FGD-RELATED 91.4 73.7 82.4 68.4 60.9 63.4 83.6	100.0 100.0 PROBLEMS WE 91.4 73.7 82.4 68.4 60.9 63.4 83.6	72.6 74.2 ERE ENCOUNTER 46.8 37.8 42.2 68.4 60.9 63.4	ED DURING T	HE MON' 720	TH OF AU	UGUST. 304	32.4 69.4
9/80 10/80	A B SYSTEM A B SYSTEM A B SYSTEM A B SYSTEM	90.6 90.6 97.4 97.4 97.4 97.3 99.3	91.6 93.7 ONS/COMMENTS NO FGD-RELATED 91.4 73.7 82.4 68.4 60.9 63.4 83.6 87.9	100.0 100.0 PROBLEMS WE 91.4 73.7 82.4 68.4 60.9 63.4 83.6 87.9	72.6 74.2 ERE ENCOUNTER 46.8 37.8 42.2 68.4 60.9 63.4 83.6 87.9	ED DURING T	HE MON' 720 744	TH OF AU	304 472	32.4 69.4

88.8

66.0 77.4

88.8

66.0

77.4

744 744 576 41.2

88.8

66.0

77.4

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

NO PROBLEMS WERE ENCOUNTERED WITH THE UNIT OR THE FGD SYSTEM DURING DEC-

1/81	SYSTEM	744
2/81	SYSTEM	672
3/81	SYSTEM	744

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION FOR THE FIRST QUARTER 1981 WAS NOT AVAILABLE AT THIS TIME.

4/81	SYSTEM	720
5/81	SYSTEM	744
6/81	SYSTEM	720

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION FOR THE SECOND QUARTER 1981 WAS NOT AVAILABLE.

7/81 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION FOR THE MONTH OF JULY WAS NOT AVAILABLE AT THIS TIME.

8/81	A B SYSTEM	87.6 99.6 93.6	56.4 50.6 53.5	100.0 100.0 100.0	56.0 50.3 53.1	744	739	395	45.0
9/81	A B SYSTEM	30.1 30.1 30.1	99.7 99.7 99.7	100.0 100.0 100.0	24.1 26.8 25.4	720	217	183	18.5

** PROBLEMS/SOLUTIONS/COMMENTS

DURING SEPTEMBER LOW SYSTEM UTILIZATION WAS DUE TO THE FACT THAT THE UNIT AND THE FGD SYSTEM WERE SHUTDOWN FOR SCHEDULED REPAIRS.

10/81	A B System	96.8 96.8 96.8	40.2 76.0 58.1	92.4 95.9 94.1	39.5 74.8 57.2	744	732	425 62.8
11/81	A B SYSTEM	99.2 99.2 99.2	95.3 56.5 75.9	98.9 98.1 98.5	74.5 44.2 59.3	720	563	427 43.4
12/81	A B SYSTEM	95.6 95.6 95.6	87.8 15.4 51.6	95.2 77.6 86.4	87.7 15.4 51.5	744	743	383 48.1

** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE FOURTH QUARTER THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED.

1/82 A 93.3 78.6 91.9 76.2

UTILITY FGD SURVEY: OCTOBER 1983 - SEPTEMBER 1984

ALABAMA ELECTRIC: TOMBIGBEE 3 (CONT.)

PERIOD	MODULE		Y OPERABILITY		UTILIZATION		PER			
	В	93.3		67.9	14.2					
	SYSTEM	93.3	46.6	79.9	45.2		744	721	336	45.7
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
			OURING JANUARY				USING /	AN UNAV	AILABI	LITY
2/82	Δ	98.7	61.8	97.9	61.8					
	В	98.7		97.2						
	SYSTEM	98.7	53.8	97.5	53.8		672	672	362	51.7
3/82	A	100.0		100.0	86.6					
	В	100.0	13.4	100.0	13.4					
	SYSTEM	100.0	50.0	100.0	50.0		744	744	372	45.1
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
			NO MAJOR FGD-P MARCH.	RELATED PROB	LEMS WERE REP	PORTED FOR T	HE MON	THS OF	FEBRUAR	DIA Y
4/82	A	98.7	63.5	97.1	41.3					
	В	98.9		96.0	26.5					
	SYSTEM	98.8	52.2	96.5	33.9		720	468	244	26.9
5/82	A	98.8	98.8	98.8	98.3					
	В	99.2	99.2	99.0	79.3					
	SYSTEM	99.0	99. 0	98.9	88.8		744	744	661	78.9
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
		t	DURING APRIL A	AND MAY NO M	AJOR FGD-RELA	TED PROBLEMS	S WERE	ENCOUN	TERED.	
6/82	SYSTEM	100.0	100.0	100.0	100.0		720	720	720	68.4
	** PROS	BLEMS/SOLUTIO	ONS/COMMENTS							
			THE UTILITY RE	PORTED THAT	NO MAJOR FGD	-RELATED PRO	BLEMS	WERE E	NCOUNTE	RED
7/82	SYSTEM	100.0	99.4	99.4	99.4		744	744	740	64.7
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
		ı	MODULE A WAS (OUT OF SERVI	CE DURING PAR	RT OF JULY D	JE TO [DAMPER I	PROBLEM	ıs.
8/82	SYSTEM	100.0	95.3	95.3	95.3		744	744	709	67.4
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
		7	THE UTILITY REDURING AUGUST	PORTED THAT	NO MAJOR FGD	-RELATED PRO	DBLEMS	WERE E	NCOUNTE	RED
9/82	SYSTEM	100.0	99.7	99.7	99.7		720	720	718	57.3
	** PRO	BLEMS/SOLUTIO	DNS/COMMENTS							_
		1	NO MAJOR FGD-F	RELATED PROB	LEMS WERE ENC	COUNTERED BY	THE UT	FILITY		
10/82	SYSTEM			100.0	100.0		744	744	74.4	7/ 7
			200.0	100.0	100.0		/44	744	744	76.3

ALABAMA ELECTRIC: TOMBIGBEE 3 (CONT.)

8/83 A 97.7 40.6

					NCE DATA UTILIZATION		PER	BOILER	FGD	CAP.
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS							
		1			LEMS WERE ENC	OUNTERED BY	THE U	TILITY		
11/82	SYSTEM	100.0	98.5	98.5	36.2		720	265	261	24.6
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS							
					THE SCRUBBER			SERVIC	E DURI	1G
12/82	SYSTEM	100.0	91.5	91.5	49.0		744	398	365	24.1
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
			10DULE A WAS NOZZLES.	OUT OF SERVI	CE DURING PAR	T OF DECEMB	ER DUE	TO PLU	GGED IN	ILET
1/83	SYSTEM	100.0	99.6	99.6	66.6		744	498	496	30.9
	** PRO	BLEMS/SOLUTIO	DNS/COMMENTS							
		7	THE UNIT WAS	SHUT DOWN DUI	RING PART OF	JANUARY FOR	A SCHI	EDULED	OUTAGE.	
			THE 3A QUENCH	ER EXPERIENC	ED LOW FLOW P	ROBLEMS DUR	ING JA	NUARY.		
2/83	SYSTEM	.0			.0		672	0	0	.0
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
		-	THE UNIT WAS	אים משסם דטאצ	RING FEBRUARY	FOR A SCHE	DULED (OUTAGE.		
3/83	SYSTEM	.0			.0		744	0	0	.0
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
		-	THE SCHEDULED	SHUTDOWN CO	NTINUED THROU	JGH MARCH.				
4/83	SYSTEM	16.1	66.5	66.5	16.3		720	177	118	14.6
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
		-	THE UTILITY R	EPORTED THAT	MAKE-UP NATE	R LINES WER	E REPA	IRED DU	RING A	PRIL.
5/83	SYSTEM	100.0	100.0	100.0	100.0		744	744	744	81.3
6/83	SYSTEM	99.9	99.4	99.4	99.4		720	720	716	78.8
	** PRO	BLEMS/SOLUTION	ONS/COMMENTS							
		t	10DULE A WAS	OUT OF SERVI	CE DURING PAR	T OF JUNE F	OR MAI	NTENANC	Ε.	
7/83	A	100.0	85.0		84.7					
	B SYSTEM	100.0	99.9 92.4		99.6 92.2		744	742	686	71.0
		BLEMS/SOLUTIO			. = . =				200	• •
		-		FDODTED THAT	NO MAJOR FGD	-DELATED DO	OBIEME	WEDE E	NCOLET	EDEN
			OURING JULY.	C. OKTED THAT	THE TIMBUR 1'60	ALEATED PR	OD LE113	MEKE E	.14000111	LKLU

40.6

UTILITY FGD SURVEY: OCTOBER 1983 - SEPTEMBER 1984

ALABAMA ELECTRIC: TOMBIGBEE 3 (CONT.)

PERIOD	MODULE AV	/AILABILIT	Y OPERABILITY F	RELIABILITY U	TILIZATION	% REMO	OVAL PART.	PER HOURS	HOURS	HOURS	CAP.
	B SYSTEM	100.0	59.5 50.1		59.5 50.1				744		63.0
	** PROBLE	EMS/SOLUTI	ONS/COMMENTS								
			MODULE A WAS OU	JT OF SERVICE	DURING PAR	T OF A	JGUST	FOR PR	RESATUR.	ATOR M	AINTEN-
9/83	A B SYSTEM	70.1 70.1 70.1	66.6		22.7 46.7 34.7			720	505	250	34.4
			ONS/COMMENTS								
	AA PROBEI	- 1137 30 20 7 1	THE UNIT WAS SE	HUT DOWN DURI	NG SEPTEMBE	R FOR	A SCH	EDULED	FALL O	JTAGE.	
7.6 /0.7											
10/83	A B	18.0 18.0	57.7 64.8		11.7 13.2						
			61.3	61.3				744	151	93	11.7
	** PROBL	EMS/SOLUT	CONS/COMMENTS								
			THE UNIT WAS DO	OWN DURING MC	ST OF OCTOR	ER FOR	A SC	HEDULE	FALL (OUTAGE.	•
11/83		77.9	69.4		69.4						
	B System	82.4 80.1	61.0 65.2	65.2	61.0 65.2			720	720	470	66.0
	** PROBL	EMS/SOLUT:	CONS/COMMENTS								
			BROKEN LIMESTO	NE FEED LINES	WERE REPOR	יטם ספדי	RING!	NOVEMB	ER.		
			A FOUR-HOUR OU STONE PREPARAT			'EMBER	FOR M	AINTENA	ANCE ON	THE L	IME-
			THE UTILITY REDUCE TO COMPUTE			MODULE	A IN	SERVI	CE DURI	4G NOVI	EMBER
			THE FGD SYSTEM THE STACK.	WAS OUT OF S	SERVICE FOR	FIVE D	AYS D	URING N	NOVEMBE	R TO DI	RY OUT
12/83		85.2	63.7		63.7						
	B SYSTEM	91.5 88.4	72.9 68.3	68.3	72.9 68.3			744	744	508	68.1
	** PROBL	EMS/SOLUT:	IONS/COMMENTS								
			THE UTILITY RE	PORTED PROBLE	EMS WITH AN	INLET	DAMPE	R AT M	DDULE A	DURIN	3
			SUB-FREEZING W DECEMBER CAUSI	EATHER CONDIT	TIONS FORCED LUGGED, AND/	THE F	GD SYS	STEM OU	JT OF S INES.	ERVICE	DURING
			SUB-FREEZING W DECEMBER CAUSI INCLEMENT WEAT SERVICE DURING	NG FROZEN, PL HER FORCED TH	LUGGED, AND/	OR BUR	STED	PIPE L	INES.		DURING
1/84	A B	74.2 25.3	DECEMBER CAUSI	NG FROZEN, PL HER FORCED TH	LUGGED, AND/	OR BUR	STED	PIPE L	INES.		DURING

PERFORMANCE DATA									
PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION	% REI	MOVAL	PER	BOILER	FGD	CAP.			
	502	PART.	HOURS	HOURS	HOURS	FACTOR			

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE ABSORBER WAS INOPERABLE DURING JANUARY DUE TO FROZEN PIPES.

MECHANICAL PROBLEMS WITH MODULE B DISCHARGE DAMPER OCCURRED IN JANUARY.

LIMESTONE FEED AND BALL MILL PROBLEMS WERE REPORTED DURING THE MONTH.

2/84	A	47.0	95.9		46.5				
	В	.0	. 0		.0				
	SYSTEM	23.5	47.9	23.2	23.2	696	337	162	22.8

** PROBLEMS/SOLUTIONS/COMMENTS

MECHANICL PROBLEMS CONTINUED ON THE MODULE B DISCHARGE DAMPER DURING FEBRUARY.

3/84	A	55.2	58.4		40.3				
	В	5 9.7	48.5		33.4				
	SYSTEM	57.5	53.4	36.8	36.8	744	513	274	40.9

** PROBLEMS/SOLUTIONS/COMMENTS

THE 3B DISCHARGE DAMPER WAS INOPERABLE IN MARCH DUE TO MECHANICAL PROBLEMS.

MODULE A WAS INOPERABLE DUE TO A PLUGGED HYDROCLONE.

4/84	A	73.8	72.6		72.5				
	В	73.8	48.8		48.7				
	SYSTEM	73.8	60.7	60.6	60.6	720	719	436	73.8

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS OUT OF SERVICE DURING PART OF APRIL TO ALLOW HOT FLUE GAS TO DRY THE STACK. WATER CARRYOVER HAD COLLECTED IN THE BASE OF THE STACK MAKING IT DIFFICULT TO MAINTAIN ADEQUATE TEMPERATURES ABOVE DEW POINT.

5/84	A	98.5	94.0		92.6				
	В	98.5	74.1		73.0				
	SYSTEM	98.5	84.1	82.8	82.8	744	733	616	73.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE ABSORBER WAS UNAVAILABLE IN MAY DUE TO THE REPLACEMENT OF MAKE-UP WATER VALVES AND THE ROTATION OF MAKE-UP WATER NOZZLES.

6/84	A	100.0	82.4		82.4			
	В	99.4	77.1		77.1			
	SYSTEM	99.7	79.7	79.7	79.7	720	720	574 67.9

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING JUNE.

7/84	SYSTEM	744
8/84	SYSTEM	744
9/84	SYSTEM	720

ALABAMA ELECTRIC: TOMBIGBEE 3 (CONT.)

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE THIRD QUARTER OF 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

-----COMPANY NAME ARIZONA ELECTRIC POWER PLANT NAME **APACHE** UNIT NUMBER COCHISE CITY STATE ARIZONA С REGULATORY CLASSIFICATION 43. (.100 LB/MMBTU) 344. (.800 LB/MMBTU) 301. (.700 LB/MMBTU) PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION NG/J 530 NET PLANT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW 195 175 NET UNIT GENERATING CAPACITY W/FGD - MW NET UNIT GENERATING CAPACITY W/FGD - TIM NET UNIT GENERATING CAPACITY WO/FGD - MW 183 EQUIVALENT SCRUBBED CAPACITY - MW ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER RILEY STOKER BOILER TYPE PULVERIZED COAL BOILER SERVICE LOAD BASE DESIGN BOILER FLUE GAS FLOW - CU.M/S 520.98 (1104000 ACFM)
BOILER FLUE GAS TEMPERATURE - C 376.7 (710 F)
STACK HEIGHT M 122. (400 FT)
STACK SHELL CONCRETE
STACK TOP DIAMETER - M 4.9 (16.2 FT) ** FUEL DATA FUEL TYPE COAL FUEL GRADE SUBBITUMINOUS 23260. (10000 BTU/LB) AVERAGE HEAT CONTENT - J/G RANGE HEAT CONTENT BTU/LB AVERAGE ASH CONTENT - % 9500-10800 15.00 RANGE ASH CONTENT % 15-20 AVERAGE MOISTURE CONTENT - % 13.00 RANGE MOISTURE CONTENT - % 9.0-15.0 AVERAGE SULFUR CONTENT - % .70 RANGE SULFUR CONTENT - %
AVERAGE CHLORIDE CONTENT % 0.4-0.6 .01 RANGE CHLORIDE CONTENT - % 0.00-0.03 *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER TYPE NONE ** ESP NUMBER 1 NUMBER OF SPARES 0 HOT SIDE AIR CORRECTION DIVISION, UOP SUPPLIER 521.0 (1104000 ACFM) 376.7 (710 F) .1 (1. IN-H2O) INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE C
PRESSURE DROP KPA .1 99.6 PARTICLE REMOVAL EFFICENCY % ** PARTICLE SCRUBBER NUMBER GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL N/A LINER GENERIC MATERIAL N/A LINER SPECIFIC MATERIAL N/A GAS CONTACTING DEVICE TYPE N/A

*** FGD SYSTEM

CAP

ACTOR

SPECIFIC TYPE

```
** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                             THROWAWAY PRODUCT
                                              WET SCRUBBING
   SO2 REMOVAL MODE
   PROCESS TYPE
                                              LIMESTONE
                                              NONE
   PROCESS ADDITIVES
                                              RESEARCH-COTTRELL
   SYSTEM SUPPLIER
                                              BURNS & MCDONNELL
   A-E FIRM
                                              FULL SCALE
   DEVELOPMENT LEVEL
                                              NEW
   NEW/RETROFIT
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.60
                                              85.00
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
   ENERGY CONSUMPTION %
                                                 4.1
   CURRENT STATUS
   COMMERCIAL START-UP
                                               1/79
                                               8/78
   INITIAL START-UP
    CONTRACT AWARDED
                                               7/74
** DESIGN AND OPERATING PARAMETERS
   DESIGN COAL SULFER CONTENT - %
                                                1.00
                                                           ( 10000 BTU/LB)
    DESIGN COAL HEAT CONTENT - J/G
                                              23260.0
   DESIGN COAL ASH CONTENT - %
                                               17.00
    DESIGN MOISTURE CONTENT - %
                                                18.00
    DESIGN CHLORIDE CONTENT - %
                                                  .00
                                              4046.7
                                                            ( 43560 SQ FT)
    SPACE REQUIREMENTS - SQ M
    OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                72.0
** QUENCHER/PRESATURATOR
    NUMBER
                                              CYCLONIC SPRAY QUENCHER
    TYPE
    SUPPLIER
                                              RESEARCH-COTTRELL
                                                188.76 ( 400000 ACFM)
132.2 ( 270 F)
    INLET GAS FLOW - CU. M/S
    INLET GAS TEMPERATURE - C
                                                  .2
    PRESSURE DROP - KPA
                                                           ( 1.0 IN-H20)
                                                            ( 9000 GPM)
    LIQUID RECIRCULATION RATE LITERS/S
                                                567.
                                                            ( 20.0 GAL/1000 ACFM)
    L/G RATIO L/CU. M
                                                 2.7
                                            CARBON STEEL
    CONSTRUCTION MATERIAL GENERIC TYPE
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                            AISI 1110
** ABSORBER
    MIMBER
                                               2
    NUMBER OF SPARES
                                               1
    GENERIC TYPE
SPECIFIC TYPE
                                              COMBINATION TOWER
                                              SPRAY/PACKED
    TRADE NAME/COMMON TYPE
                                              N/A
    SUPPLIER.
                                              RESEARCH-COTTRELL
    DIMENSIONS - FT
                                              30.0 DIA X 110.0
    SHELL GENERIC MATERIAL
                                              CARBON STEEL
    SHELL SPECIFIC MATERIAL
                                              AISI 1110
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                              N/A
    LINER GENERIC MATERIAL
                                              ORGANIC
    LINER SPECIFIC MATERIAL
                                              GLASS FLAKE-FILLED POLYESTER
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                             FLAKELINE 103
    GAS CONTACTING DEVICE TYPE
                                              SFRAY ZONE & VERTICAL CROSS CHANNEL FIXED GRID P
    NUMBER OF CONTACTING ZONES
                                              2
                                              567.
    LIQUID RECIRCULATION RATE - LITER/S
                                                            ( 9000 GPM)
    L/G RATIO L/CU.M
                                                5.3
                                                            ( 40.0 GAL/1000 ACF)
    GAS-SIDE PRESSURE DROP - KPA
                                                            ( 2.5 IN-H20)
                                                  .6
    SUPERFICAL GAS VELOCITY - M/SEC
                                                  3.0
                                                             ( 10.0 FT/S)
    INLET GAS FLOW - CU. M/S
                                                 94.38
                                                             ( 200000 ACFM)
    INLET GAS TEMPERATURE C
                                                68.3
                                                             ( 155 F)
    SO2 REMOVAL EFFICIENCY - %
                                                 97.0
    PARTICLE REMOVAL EFFICENCY %
                                                 99.6
** MIST ELIMINATOR
    PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                              PRIMARY COLLECTOR
    NUMBER PER SYSTEM
                                               2
    NUMBER OF SPARES PER SYSTEM
                                               1
    NUMBER PER MODULE
    GENERIC TYPE
                                              IMPINGEMENT
```

BAFFLE

```
CLOSED VANE
   TRADE NAME/COMMON TYPE
                                             MUNTERS
   MANUFACTURER
                                              HORIZONTAL
   CONFIGURATION
   NUMBER OF STAGES
                                                  2
   NUMBER OF PASSES PER STAGE
                                                  3
                                                            ( 2.0 FT)
   FREEBOARD DISTANCE - M
                                                  .61
                                                30.48
                                                            (12.0 IN)
   DISTANCE BETWEEN STAGES - CM
                                                10.2
                                                            ( 4.00 IN)
   DISTANCE BETWEEN VANES - CM
   VANE ANGLES - DEGREES
                                                45
                                                            ( 1.0 IN-H20)
   PRESSURE DROP - KPA
                                                  . 2
   SUPERFICAL GAS VELOCITY - M/S
                                                 3.0
                                                            ( 10.0 FT/S)
                                             ORGANIC
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              POLYVINYL CHLORIDE
   CONSTRUCTION MATERIAL SPECIFIC TYPE
   WASH WATER SOURCE
                                              FRESH
                                              INTERMITTENT [LOWER STAGE]; ONCE EVERY HOUR [UPP
   WASH FREQUENCY
   WASH RATE - L/S
                                                12.6 ( 200 GAL/MIN)
** REHEATER
   NUMBER
                                               0
   GENERIC TYPE
                                              NONE
                                              N/A
   SPECIFIC TYPE
   TRADE NAME/COMMON TYPE
                                              N/A
                                               50.0
   PERCENT GAS BYPASSED - AVG
   TEMPERATURE INCREASE C
                                                           ( 78 F)
                                                43.3
                                               46.1
   INLET FLUE GAS TEMPERATURE - C
                                                           ( 115 F)
( 193 F)
   OUTLET FLUE GAS TEMPERATURE - C
                                                89.4
   CONSTRUCTION MATERIAL GENERIC TYPE
                                             NONE
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                             N/A
** FANS
   NUMBER
                                               2
   NUMBER OF SPARES
                                               0
                                              CENTRIFUGAL
   DESIGN
   SUPPLIER
                                              WESTINGHOUSE
   FUNCTION
                                              UNIT
   APPLICATION
                                              FORCED DRAFT
   SERVICE
                                              DPY
   FLUE GAS FLOW RATE - CU.M/S
                                              188.76
                                                            ( 400000 ACFM)
                                                            ( 270 F)
   FLUE GAS TEMPERATURE - C
                                               132.2
   PRESSURE DROP - KPA
                                                 6.2
                                                            (20.5 IN-H20)
                                            CARBON STEEL
   CONSTRUCTION MATERIAL GENERIC TYPE
** DAMPERS
   NUMBER
    FUNCTION
                                              SHUT-OFF
                                              LOUVER
    GENERIC TYPE
    SPECIFIC TYPE
                                              PARALLEL BLADE MULTILOUVER
                                              OPEN/CLOSED
   MODULATION
    SEAL AIR FLOW - CU. M/S
                                                   .24
                                                            ( 500 ACFM)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                              CARBON STEEL
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                             NR
    LINER GENERIC MATERIAL TYPE
                                              NONE
    LINER SPECIFIC MATERIAL TYPE
                                              N/A
** DAMPERS
   NUMPER
                                               2
    FUNCTION
                                              SHUT-OFF
                                              GUILLOTINE
    GENERIC TYPE
    SPECIFIC TYPE
                                              TOP-ENTRY GUILLOTINE
                                              OPEN/CLOSED
   MODULATION
    SEAL AIR FLOW - CU. M/S
                                                             ( 500 ACFM)
                                                  .24
                                             CARBON STEEL
    CONSTRUCTION MATERIAL GENERIC TYPE
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              NR
    LINER GENERIC MATERIAL TYPE
                                              HIGH ALLOY
   LINER SPECIFIC MATERIAL TYPE
                                             NICKEL BASE/CHROMIUM-IRON-COPPER-MOLYBDENUM
** DAMPERS
   NUMBER
   FUNCTION
                                              SHUT-OFF
   GENERIC TYPE
                                              LOUVER
   SPECIFIC TYPE
                                              PARALLEL BLADE MULTILOUVER
```

OPEN/CLOSED MODULATION SEAL AIR FLOW - CU. M/S .24 (500 ACFM) CARBON STEEL CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE NR LINER GENERIC MATERIAL TYPE HIGH ALLOY NICKEL BASE/CHROMIUM-IRON-COPPER-MOLYBDENUM LINER SPECIFIC MATERIAL TYPE ** DUCTWORK ABSORBER INLET LOCATION RECTANGULAR CONFIGURATION 12.0 X 14.0 DIMENSIONS SHELL GENERIC MATERIAL TYPE CARBON STEEL AISI 1110 SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DUCTWORK LOCATION ABSORBER OUTLET CONFIGURATION RECTANGULAR DIMENSIONS 12.0 X 14.0 SHELL GENERIC MATERIAL TYPE CARBON STEEL SHELL SPECIFIC MATERIAL TYPE AISI 1110 LINER GENERIC MATERIAL TYPE ORGANIC LINER SPECIFIC MATERIAL TYPE FLUOROELASTOMER ** REAGENT PREPARATION EQUIPMENT FUNCTION WET BALL MILL DEVICE COMPARTMENTED DEVICE TYPE NR MANUFACTURER KENNEDY VAN SAUN NUMBER 1 NUMBER OF SPARES O FULL LOAD DRY FEED CAPACITY - M.TONS/HR 4.5 (5 TPH) PRODUCT QUALITY - % SOLIDS 45.0 ** TANKS SERVICE NUMBER ----------ABSORBER FEED 1 REAGENT FEED 1 MILL SLURRY SUMP 1 WASTE SLURRY SUMP 1 ** PUMPS SERVICE NUMBER -----ABSOPBER 3 QUENCHER 4 MILL SLURRY RECYCLE ADDITIVE FEED 2 WASTE SLURRY TRANSFER ** SOLIDS CONCENTRATING/DEWATERING DEVICE NONE *** SLUDGE MOISTURE CONTENT - % TOTAL FREE WATER 70.0 % CASO4 DRY 80 0 ** TREATMENT METHOD NONE DEVICE N/A PROFRIETARY PROCESS N/A ** DISPOSAL NATURE FINAL TYFE DUNG LOCATION OFF-SITE SITE TRANSPORTATION METHOD PIPELINE

** PROCESS CONTROL AND INSTRUMENTATION

SITE TREATMENT NONE

SITE DIMENSIONS 25 TO 30 ACRES BY 18 FT DEEP SITE CAPACITY - CU.M 611500 (500.0 ACRE-FT)

SITE SERVICE LIFE - YRS

PROCESS STREAM QUENCHER RECYCLE LINE

CHEMICAL PARAMETERS

PHYSICAL VARIABLES PERCENT SOLIDS

CONTROL LEVELS 5.0 PH
PROCESS CONTROL MANNER MANUAL
PROCESS CHEMISTRY MODE FEEDBACK

** WATER BALANCE

WATER LOOP TYPE OPEN

MAKEUP WATER ADDITION - LITERS/S 115.9 (1840 GPM)

SOURCE OF MAKEUP WATER WELL WATER

** CHEMICALS AND CONSUMPTION

FUNCTION ABSORBENT
NAME LIMESTONE
PRINCIPAL CONSTITUENT >93% CACO3
SOURCE/SUPPLIER PAUL LIME
UTILIZATION - % 99.0
POINT OF ADDITION BALL MILL

** FGD SPARE CAPACITY INDICES

ABSORBER % 100.0
MIST ELIMINATOR - % .0
FAN - % .0
BALL MILL - % .0
EFFLUENT HOLD TANK - % .0
RECIRCULATION PUMP - % 50.0

** FGD SPARE COMPONENT INDICES

ABSORBER 1.0
MIST ELIMINATOR .0
FAN .0
BALL MILL .0
EFFLUENT HOLD TANK .0
RECIRCULATION PUMP 1.0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

8/78 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

INITIAL OPERATIONS BEGAN IN AUGUST WITH THE BOILER AND SCRUBBER SYSTEM FOR TESTING PURPOSES.

9/78 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

SCRUBBER AND BOILER TESTING CONTINUED THROUGH SEPTEMBER. FINAL FACILITY CONSTRUCTION SHOULD BE COMPLETE BY OCTOBER.

10/78 SYSTEM 744 303 59.5

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS SHUTDOWN IN EARLY OCTOBER TO MAKE ADDITIONAL BOILER MODIFICATIONS. NO PROBLEMS WERE REPORTED FOR THE FGD SYSTEM. COMPLIANCE TESTING IS SCHEDULED FOR EARLY NOVEMBER. THE UTILITY HAS DECIDED THAT IN APPROXIMATELY A YEAR THE SCRUBBER INLET DUCTWORK WILL BE CHANGED FROM CARBON

ARIZONA ELECTRIC POWER: APACHE 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.
SO2 PART. HOURS HOURS FACTOR

SUL TART, MODES MO

STEEL TO STAINLESS STEEL.

11/78 A 24.8 16.8 B 43.7 29.6

SYSTEM 68.5 46.4 720 488 334 82.8

** PROBLEMS/SOLUTIONS/COMMENTS

THE SO2 STACK MONITORS HAVE NEVER BEEN OPERABLE. THE MONITORS HAVE BEEN SENT BACK TO THE FACTORY AND ARE NOT EXPECTED BACK ON SITE UNTIL LATE DECEMBER.

THE LIMESTONE CRUSHER HAS BEEN UNABLE TO OPERATE AT DESIGN CAPACITY.

A COMPLIANCE TEST WAS COMPLETED BUT THE RESULTS ARE NOT YET AVAILABLE. THE ACCEPTANCE IS SCHEDULED FOR THE BEGINNING OF 1979.

12/78 SYSTEM .0 .0 744 512

** PROBLEMS/SOLUTIONS/COMMENTS

RESULTS OF THE RECENT COMPLIANCE TEST INDICATED THAT SO2 EMISSIONS WERE BETWEEN 1.2 LB/MM BTU, THE FEDERAL APPLICABLE STANDARD; AND 0.8 LB/MM BTU, THE STATE STANDARD, WITHOUT THE FGD SYSTEM. THE UTILITY IS CURRENTLY BURNING LOW SULFUR COAL (0.6% S). IT IS BELIEVED THAT THE STATE STANDARD COULD BE MET WITHOUT FGD SYSTEM OPERATION WHEN THE FURNACE IS "FINE TUNED".

A 30 HOUR OUTAGE OCCURRED DUE TO A RUPTURE IN THE REAGENT FEED LINE.

1/79 SYSTEM .0 .0 744 662 0

** PROBLEMS/SOLUTIONS/COMMENTS

SHAKEDOWN/DEBUGGING OPERATION CONTINUED THROUGH JANUARY.

COMMERCIAL OPERATIONS BEGAN ON JANUARY 15.

2/79 SYSTEM .0 .0 672 504 0

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS NOT IN SERVICE DURING DECEMBER, JANUARY, OR FEBRUARY DUE TO VARIOUS SHAKEDOWN/DEBUGGING PROBLEMS ESPECIALLY IN MAINTAINING RECYCLE PUMP OPERATION.

3/79 SYSTEM .0 .0 744 372 0

** PROBLEMS/SOLUTIONS/COMMENTS

A BOILER EXPLOSION AT THE BURNER FACE CAUSED THE UNIT TO BE DOWN FROM THE LAST WEEK IN FEBRUARY THROUGH THE MIDDLE OF MARCH.

4/79 SYSTEM 720 720

** PROBLEMS/SOLUTIONS/COMMENTS

COMPLIANCE TESTS WERE RUN ON THIS UNIT LAST NOVEMBER AND THE UNIT WAS DECLARED COMMERCIAL IN FEBRUARY. THE FGD SYSTEM OPERATES ONLY ABOUT 50 % OF THE BOILER HOURS BECAUSE THE UNIT OPERATES AT SUCH A LOW RATING 50% OF THE TIME THAT THE FGD SYSTEM IS NOT NEEDED.

5/79 SYSTEM 744

6/79 SYSTEM 720

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

IN GENERAL THE FGD SYSTEM AND BOILER OPERATED WELL THROUGH MAY AND JUNE.

THE FRP REAGENT FEED PIPING HAS BEEN A CONTINUAL PROBLEM AREA. THE FRP HAS BEEN RUPTURING PARTICULARLY AT PIPING CONNECTIONS. THE UTILITY IS IN THE PROCESS OF REPLACING THE FRP PIPING WITH CARBON STEEL PIPING.

THE BALL MILL APPEARS TO HAVE BEEN UNDERDESIGNED. THE MILL PRODUCES 4 TONS/HOUR OF GROUND LIMESTONE AT BEST ALTHOUGH IT WAS RATED AT 5 TON/HOUR CAPACITY.

7/79 SYSTEM 744

8/79 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED HAVING EXTENSIVE PROBLEMS WITH THE REAGENT HANDLING SYSTEM PARTICULARLY WITH RESPECT TO FEED LINE FAILURES, PIPING PLUGGING AND GRINDING OPERATIONS. THE REAGENT HANDLING SYSTEM ACCOMODATES BOTH UNITS 2 AND 3.

9/79 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE THIRD QUARTER OF 1979 THE BOILER AND FGD SYSTEM ONLY OPERATED ABOUT 25% OF THE TIME BECAUSE OF CONTINUING PROBLEMS WITH THE REAGENT FEED LINE. THE FRP SECTION FROM THE GRINDER TO THE SCRUBBERS FAILED. THE LINE WAS REPAIRED AT THE END OF SEPTEMBER.

ON NOVEMBER 3 THE UNIT WILL BE SHUT DOWN FOR A FOUR TO SIX WEEK SCHEDULED OUTAGE.

10/79 SYSTEM .0 .0 .0 744 0

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY IS IN THE PROCESS OF REPLACING THE REAGENT HANDLING SYSTEM; THEREFORE, THE FGD SYSTEM DID NOT OPERATE DURING OCTOBER.

11/79 SYSTEM 100.0 100.0 100.0 6.3 720 41 41 2.9

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS OUT OF SERVICE FOR MOST OF NOVEMBER FOR AN ANNUAL INSPECTION.

12/79 SYSTEM 100.0 .0 .0 .0 744 130 0 5.7

** PROBLEMS/SOLUTIONS/COMMENTS

THE EXTENSIVE PROBLEMS ENCOUNTERED EARLIER WITH THE REAGENT HANDLING SYSTEM HAVE BEEN RESOLVED. THE SYSTEM REPLACEMENT WAS COMPLETED IN DECEMBER.

DURING DECEMBER THE BOILER OPERATED 130 HOURS FOR WHICH THE SCRUBBER WAS AVAILABLE 100% OF THE TIME.

THE BOILER ENCOUNTERED DAMPER PROBLEMS THAT ACCOUNTED FOR MOST OF THE DECEMBER DOWN TIME.

1/80 SYSTEM 91.0 58.3 88.8 57.3 744 731 426 56.1

ARIZONA ELECTRIC POWER: APACHE 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

DURING JANUARY SOME OUTAGE TIME WAS DUE TO A PUMP MALFUNCTION.

OUTAGE TIME WAS ALSO CAUSED BY A BROKEN FEED BELT TO THE LIMESTONE BALL

MILL.

2/80 SYSTEM 92.8 96.7 92.8 92.8 696 668 646 87.4

** PROBLEMS/SOLUTIONS/COMMENTS

DURING FEBRUARY OUTAGE TIME RESULTED FROM AN ESP FAILURE.

FORCED OUTAGE TIME WAS ALSO CAUSED BY A PUMP MALFUNCTION.

3/80 SYSTEM 99.1 99.1 99.0 99.1 744 744 738 74.1

** PROBLEMS/SOLUTIONS/COMMENTS

SOME OF THE OUTAGE TIME DURING MARCH OCCURRED BECAUSE OF PUMP FAILURES.

OUTAGE TIME RESULTED FROM STICKING VALVES AND LIMESTONE FEED-BELT

PROBLEMS.

4/80 SYSTEM 67.2 65.2 65.2 61.4 720 678 442

** PROBLEMS/SOLUTIONS/COMMENTS

DURING APRIL THE FGD SYSTEM WAS FORCED DOWN DUE TO PUMP FAILURES AND A

RUPTURE IN THE SLURRY RECIRCULATION LINE.

5/80 SYSTEM 90.5 90.5 90.5 744 744 673

** PROBLEMS/SOLUTIONS/COMMENTS

DURING MAY THE UNIT WAS FORCED OFF LINE WHEN THE LIMESTONE CRUSHER

MALFUNCTIONED.

THE UNIT WAS ALSO FORCED OUT DUE TO PUMP AND VALVE FAILURES.

6/80 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE DATA FOR THE MONTH OF JUNE HAS BEEN

MISPLACED.

7/80 202 100.0 .0 .0

203 85.0 85.7 85.0 85.7 85.0 SYSTEM 100.0 85.7 85.7 85.0

** PROBLEMS/SOLUTIONS/COMMENTS

MODULE 202 WAS AVAILABLE THE ENTIRE MONTH, BUT WAS NOT OPERATED.

THE FGD SYSTEM WAS DOWN IN JULY BECAUSE OF A CIRCUIT BREAKER MALFUNCTION.

744

738

633 77.8

FAILURE OF BOTH THE BYPASS DAMPER AND THE PACKING PUMP ALSO CAUSED OUTAGE TIME DURING THE MONTH.

YSTEM 96.8 66.0 95.2 63.3 744 714 471 61.0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

TOWER 202 WAS UNAVAILABLE IN AUGUST BECAUSE OF THE LINER BEING REPLACED.

A SAMPLE LINE FAILURE CAUSED TOWER 203 TO GO DOWN FOR 24 HOURS.

THE OPERATION OF THE FGD SYSTEM WAS REDUCED BECAUSE OF LOW LOAD CAPACITY.

9/80 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

NO INFORMATION WAS AVAILABLE FOR SEPTEMBER 1980.

10/80	202	. 0	.0		.0				
	203	92.6	87.7	9 8.6	82.4				
	SYSTEM	92.7	87.7	98.6	82.4	744	699	613	62.4

** PROBLEMS/SOLUTIONS/COMMENTS

MODULE 202 WAS NOT OPERATED DURING THE MONTH OF OCTOBER DUE TO A SCHEDULED ANNUAL OVERHAUL.

DURING OCTOBER FORCED OUTAGES OCCURRED AS A RESULT OF PH INSTABILITY IN THE SYSTEM.

THE LOSS OF OPERATION TIME ON MODULE 203 WAS PRIMARILY DUE TO REDUCED LOAD CAPACITY DURING OCTOBER.

11/80	202	20.0	22.4	40.0	6.7				
	203	. 0	.0		. 0				
	SYSTEM	20.0	22.4	40.0	6.7	720	214	48 2	5.1

** PROBLEMS/SOLUTIONS/COMMENTS

DURING NOVEMBER THE BOILER WAS NOT IN SERVICE THE FIRST 21 DAYS. THE BOILER WAS OPERATED AT REDUCED LOAD FOR THE FIRST 96 HOURS AFTER STARTUP UNTIL THE FGD SYSTEM WAS ON-LINE.

FAILURE OF THE LIMESTONE BALLMILL ACCOUNTED FOR 72 HOURS OF OUTAGE TIME.

12/80	202	100.0	100.0	100.0	99.9			
	203	.0	.0		. 0			
	SYSTEM	100.0	100.0	100.0	99.9	74	4 743	743 87.

** PROBLEMS/SOLUTIONS/COMMENTS

NO FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE MONTH OF DECEMBER.

1/81	202	100.0	62.9	100.0	62.9				
	203	.0	.0		.0				
	SYSTEM	100.0	62.9	100.0	62.9	744	744	468	86.6

** PROBLEMS/SOLUTIONS/COMMENTS

MODULE 202 WAS NOT OPERATED DURING THE LAST 276 HOURS OF THE MONTH AS A RESULT OF THE LOW SULFUR CONTENT OF THE COAL BEING FIRED.

MODULE 203 WAS NOT AVAILABLE FOR OPERATION DURING JANUARY.

2/81	202	100.0	10.7	100.0	10.7			
	203	. 0	.0		. 0			
	SYSTEM	100.0	10.7	100.0	10.7	672	672	72 77.4

ARIZONA ELECTRIC POWER: APACHE 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS FACTOR ** PROBLEMS/SOLUTIONS/COMMENTS DURING FEBRUARY THE OPERATION OF THE FGD SYSTEM WAS REDUCED DUE TO THE LOW SULFUR CONTENT OF THE COAL. REPAIRS WERE MADE ON TOWER 203 DURING FEBRUARY. .0 3/81 202 .0 100.0 43.7 100.0 53.7 203 325 70.2 100.0 100.0 43.7 744 605 SYSTEM 53.6 ** PROBLEMS/SOLUTIONS/COMMENTS DURING MARCH MODULE 202 WAS NOT AVAILABLE DUE TO EROSION PROBLEMS. THE SYSTEM WAS BY-PASSED DURING PART OF THE MONTH BECAUSE THE UNIT WAS FIRING LOW SULFUR COAL. 4/81 202 .0 . 0 . 0 203 100.0 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 100.0 720 720 720 98.2 ** PROBLEMS/SOLUTIONS/COMMENTS DURING APRIL MODULE 202 WAS NOT AVAILABLE FOR OPERATION DUE TO ERROSION OF THE BOWL AREA OF THE MODULE. THIS HAS BEEN A CONTINUAL PROBLEM AND THE UTILITY IS PRESENTLY CONDUCTING STUDIES TO ALLEVIATE THE PROBLEM. 5/81 202 100.0 . 0 . 0 100.0 100.0 100.0 203 100.0 SYSTEM 100.0 100.0 100.0 100.0 744 744 744 87.4 ** PROBLEMS/SOLUTIONS/COMMENTS DURING MAY THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED.

MODULE 202 WAS AVAILABLE THE ENTIRE MONTH, BUT WAS NOT OPERATED.

6/81 202 100.0 .0 . 0 203 100.0 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 100.0 720 716 720 91.9

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR PROBLEMS WERE EXPERIENCED DURING THE MONTH OF JUNE.

7/81 202 100.0 45.2 100.0 45.2 203 46.2 46.2 100.0 46.2 SYSTEM 100.0 91.4 100.0 91.4 744 744 680 91.0

** PROBLEMS/SOLUTIONS/COMMENTS

MODULE 203 WAS TAKEN OUT OF SERVICE ON JULY 15 FOR PREVENTIVE MAINTENANCE AND REPAIRS, AT WHICH TIME MODULE 202 WAS PUT INTO SERVICE.

8/81 202 100.0 39.9 100.0 35.5 203 .0 ٠.0 SYSTEM 100.0 39.9 100.0 35.5 744 661 264 75.2

720

718

713 85.4

PERFORMANCE DAT	۵					
PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZ	ATION % RE	MOVAL	PER	ROILER	FGU	CAP.
	502	PART.	HOURS	HOURS	HOURS	FACTOR
	302	10011	110010	11001.0	110010	1 70 101

** PROBLEMS/SOLUTIONS/COMMENTS

MODULE 202 WAS REMOVED FROM SERVICE ON AUGUST 8 AS A RESULT OF PROBLEMS ENCOUNTERED WITH THE ELECTROSTATIC PRECIPITATOR. THE MODULE WAS PLACED BACK IN SERVICE ON AUGUST 21.

9/81 20	2 100	0.0 9	9.3	100.0	99.0
20	13	.0	.0		.0
SY	STEM 100	0.0 9	9.3	100.0	99.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE ONLY PROBLEMS ENCOUNTERED DURING THE MONTH WERE BOILER RELATED.

10/81	202	100.0	100.0	100.0	41.5				
	203	. 0	.0		.0				
	SYSTEM	100.0	100.0	100.0	41.5	744	303	309	29.2

** PROBLEMS/SOLUTIONS/COMMENTS

UNIT 2 WAS DOWN FROM OCTOBER 3 UNTIL OCTOBER 20 FOR ANNUAL MAINTENANCE AND REPAIRS.

11/81	202	65.4	63.6	64.8	63.6				
	203	.0	. 0		.0				
	SYSTEM	65.4	63.6	64.8	63.6	720	720	458	74.2

** PROBLEMS/SOLUTIONS/COMMENTS

MODULE 202 WAS TAKEN OUT OF SERVICE TWICE DURING NOVEMBER BECAUSE OF LOW SLURRY DENSITY.

ON NOVEMBER 22 THE SYSTEM WAS TAKEN OUT OF SERVICE FOR THE REMAINDER OF THE MONTH FOR REPAIRS ON THE DAMPER SEALS.

ADDITIONAL OUTAGE TIME DURING THE MONTH WAS DUE TO BOILER-RELATED PROBLEMS.

12/81 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE ORIGINAL COPY OF THE DECEMBER UPDATE INFORMATION WAS LOST IN THE MAIL.

1/82	202	80.5	90.5	80.5	80.5				
	203		. 0		.0				
	SYSTEM	80.5	90.5	80.5	80.5	744	662	599	70.9

** PROBLEMS/SOLUTIONS/COMMENTS

DURING JANUARY MODULE 202 WAS DOWN APPROXIMATELY 145 DUE TO RESTRICTIONS IN A FEED LINE.

2/82	202		.0		.0				
	203	98.6	96.2	99.0	96.2				
	SYSTEM	98.6	96.2	99. 0	96.2	672	672	646	81.3

** PROBLEMS/SOLUTIONS/COMMENTS

DURING FEBRUARY MODULE 202 WAS DOWN FOR REPAIRS AND MAINTENANCE.

MODULE 203 WAS OUT OF SERVICE FOR APPROXIMATELY SIX HOURS DUE TO A QUENCHER PUMP FAILURE.

ERIOD	MODULE AV	AILABILI	TY OPERABILIT	Y RELIABILITY	UTILIZATION	502	PART.	HOURS	HOURS		
3/82	202		. 0		۰.0						
J, J,	203	100.0	99.0	100.0	87.3						
	SYSTEM	100.0	99.0	100.0	87.3			744	656	649	50.0
	** PROBLE	MS/SOLUT	IONS/COMMENTS								
			DURING MARCH 2 WATER WALL	MODULE 203 WARUPTURE.	AS OUT OF SER	RVICE P	ART OF	THE 1	TIME DU	E TO A	UNIT
/82	202	100.0			.0						
	203	87.2			87.2 87.2			700	700		
	SYSTEM	87.2	87.2	87.2	87.2			720	720	627	70.1
	** PROBLE	MS/SOLUT	IONS/COMMENTS								
			DURING APRIL	OUTAGE TIME I	FOR MODULE 20	O3 WAS	DUE TO	PUMP	PROBLE	15.	
/82	202	3.9		100.0							
	203 SYSTEM	.0 3.9	.0 5.3	100.0	.0 3.9			744	541	29	48.6
	** PROBLE	MS/SOLUT	IONS/COMMENTS							•	
				AS UNAVAILABLE	S BURTUS MAY	DUE TO	5045 N	44 100			
			STRUCTION.			002 10	SUME I	IAJUR	REPAIRS	ANU R	ECUN-
/82	202	100.0	97.0 .0	100.0	97.0						
	SYSTEM	100.0	97.0	100.0	.0 97.0			720	720	698	82.3
	** PROBLE	MS/SOLUT	IONS/COMMENTS								
			THE UTILITY F	REPORTED THAT	NO MAJOR FGD	D-RELAT	ED PROE	SLEMS	WERE EN	1COUNTE	RED
7/82	202	100.0	_	100.0	20.0						
, 02	203	700 0	•		•						
	SYSTEM	100.0	99.9	100.0	99.9			744	744	743	85.1
	** PROBLE	MS/SOLUT	IONS/COMMENTS								
			NO MAJOR FGD- DURING JULY.	-RELATED PROBI	LEMS WERE ENC	COUNTER	ED BY 1	THE UT	TILITY		
3/82	202	100.0	98.4	100.0	07.7						
, 02	203	100.0	.0	100.0	87.3 .0						
	SYSTEM	100.0	98.4	100.0	87.3			744	660	650	79.3
	** PROBLE	MS/SOLUT	IONS/COMMENTS								
			THE UTILITY R	REPORTED THAT	NO MAJOR FGD	D-RELAT	ED PROE	BLEMS	WERE EN	VCOUNTE	RED
/82	202	100.0	87.7	100.0	87.7						
	203	100.0	. 0	2	.0						
	SYSTEM	100.0	87.7	100.0	87.7			720	72 0	631	73.2
	** PROBLE	MS/SOLUT	IONS/COMMENTS								
			THE UTILITY R	REPORTED THAT	NO MAJOR FGO	D-RELAT	ED PROE	BLEMS	WERE E	4COUNTE	RED
/82	202	100.0	100.0	100.0	2.9						
					·/						

				TY RELIABIL	RMANCE DATA ITY UTILIZATI	ON % REI	MOVAL PART.	PER HOURS	HOURS	HOURS	FACTOR
	203	100.0	.0		.0						
	SYSTEM			100.0	2.9			744	22	22	2.0
	** PROBL	EMS/SOLUTI	CONS/COMMENT	s							
			ON OCTOBER	1 THE UNIT 1	WAS DOWN FOR	ANNUAL M	AINTEN.	ANCE A	ND REPA	IR OUT	AGES.
11/82	202	100.0	.0		.0						
	203	19.4	31.1	94.4				700	417		15.1
	SISIEM	19.4	31.1	94.4	9.4			720	217	68	15.1
	** PROBL	EMS/SOLUT	IONS/COMMENT	S							
				S PUT ON LI	NE NOVEMBER 2 OUTAGE.	AFTER	THE CO	MPLETI	ON OF A	NNUAL	
			MODULE 203	WAS PLACED	BACK IN SERVI	CE ON NO	VEMBER	24.			
12/82	202	100.0	.0		.0						
	203	90.2	68.8		68.8						
	SYSTEM	90.2	68.8	87.6	68.8			744	744	512	65.1
	** PROBL	EMS/SOLUT	IONS/COMMENT	·s							
			THE UTILITY DURING DECE		NO MAJOR	FGD-RELA	TED PR	OBLEMS	WERE E	NCOUNT	ERED
1/83	202	100.0			.0						
	203 SYSTEM		68.7 68.7	100.0 100.0	64.2 64.2	.5		744	6.04	478	57.2
					04.2			/ + +	0 70	470	37.2
	** PROBL	EMS/SOLUT	IONS/COMMENT	S							
			NO MAJOR FO		ROBLEMS WERE	ENCOUNTE	RED				
2/83	202	100.0	. 0		.0						
	203 System	99.9 99.9		99.8	61.8 61.8			672	672	415	62.4
					91.0			672	672	413	02.4
	** PROBL	.EMS/SOLUT	IONS/COMMENT	rs							
			NO MAJOR FO	_	ROBLEMS WERE	REPORTED	BY TH	E UTIL	ITY		
3/83	202	100.0	.0		.0						
	203 SYSTEM	98.8 98.8	56.1 56.1	95.1 95.1				744	711	174	25.2
				•	23.4			/ 77	, 311	1/4	23.2
	** PRUBL	.EMS/SULUT	IONS/COMMENT		FROM MARCIL 1	TO MARCH		· TO 1	O DEW	L ID	
			THE ONT! W	AS OFF LINE	FROM MARCH 1	IU MARCH	17 00	IE 10 L	.UW DEMA	, UN.	
4/83	202	100.0	.0		.0						
	203 SYSTEM	99.2 99.2	54.4 54.4	98.5 98.5				720	720	392	54.1
			IONS/COMMENT						, , ,		
	אה דאטטנ	.E.13/ 3ULUT			ROLAM ON TAH	FGD-RELA	TED PR	OBLEMS	WERE F	NCOUNT	ERED
			DURING APR				=				
5/83	202	100.0	.0		.0						

	MODULE	AVAILABILIT	Y OPERABILITY	RELIABILITY	UTILIZATION	% REMOVAL SO2 PART.	HOURS		HOURS	
	203	99.7	42.3	99.4	42.3					
	SYSTEM	99.7	42.3	99.4	42.3		744	744	315	50.3
	** PROB	LEMS/SOLUT	CONS/COMMENTS							
			THE UTILITY FOURING MAY.	EPORTED THAT	NO MAJOR FGD	-RELATED PRO	BLEMS	WERE EI	NCOUNTE	RED
6/83	202	100.0	. 0		.0					
	203		26.9		8.5					
	SYSTEM	100.0	26.9	100.0	8.5		720	229	62	13.7
	** PROB	LEMS/SOLUTI	CONS/COMMENTS							
			UNIT 2 WAS TA	KEN OFF LINE	ON JUNE 10 A	AS A RESULT C	F LOW	DEMAND	•	
7/83	202	90.3			1.4					
	203 SYSTEM		49.2 51.5		29.4 30.8		744	445	220	35.9
		100.0	31.3	100.0	30.6		/44	445	229	35.7
8/83	202	100.0	.0		.0					
	203 SYSTEM	100.0 100.0	75.6 75.6	100.0 100.0	13.6 13.6		744	176	101	12 7
		100.0	75.0	100.0	13.6		/44	134	101	12.3
9/83	202	100.0			7.9					
	203 SYSTEM	99.9 100.0	42.2 50.1	99.7 100.0	42.0		700	710	7/0	F0.3
			ONS/COMMENTS		49.9		720	718	360	59.1
	** FRUE	JEE 137 30 EU 1	LONS/COMMENTS		د.					
					NO MAJOR FGD ROUGH SEPTEMB		BLEMS	WERE EN	NCOUNTE	RED
0/83	202	100.0					BLEMS	WERE EN	NCOUNTE	RED
0/83	203	100.0	FOR THE PERIO		ROUGH SEPTEMB .0 .0				NCOUNTE	RED
0/83		100.0	FOR THE PERIO		ROUGH SEPTEMB .0		BLEMS 744			
0/83	203 SYSTEM	100.0	FOR THE PERIO		ROUGH SEPTEMB .0 .0					
0/83	203 SYSTEM	100.0	FOR THE PERIO .0 .0 .0 CONS/COMMENTS	OD OF JULY TH	ROUGH SEPTEMB .0 .0	SER, 1983.	744 RE MON	47 /TH OF (0 DCTOBER	1.0
	203 SYSTEM ** PROB	100.0	FOR THE PERIO .0 .0 .0 CONS/COMMENTS THE UTILITY F EXCEPT FOR OC	OD OF JULY TH	ROUGH SEPTEMB .0 .0 .0 .0	SER, 1983.	744 RE MON	47 /TH OF (0 DCTOBER	1.0
	203 SYSTEM ** PROB	100.0 100.0 BLEMS/SOLUTI	FOR THE PERIO .0 .0 .0 CONS/COMMENTS THE UTILITY F EXCEPT FOR OC	OD OF JULY TH	ROUGH SEPTEMB .0 .0 .0 .0 UNIT 2 WAS D CTOBER 3. AN .0	SER, 1983.	744 RE MON	47 /TH OF (0 DCTOBER	1.0
	203 SYSTEM ** PROB 202 203 SYSTEM	100.0 100.0 BLEMS/SOLUTI	FOR THE PERIO .0 .0 .0 CONS/COMMENTS THE UTILITY F EXCEPT FOR OC OCTOBER 15.	OD OF JULY TH	ROUGH SEPTEMB .0 .0 .0 .0 .0 UNIT 2 WAS D CTOBER 3. AN	SER, 1983.	744 RE MON	47 /TH OF (0 DCTOBER	1.0
	203 SYSTEM ** PROB 202 203 SYSTEM	100.0 100.0 BLEMS/SOLUTI	FOR THE PERIO .0 .0 .0 IONS/COMMENTS THE UTILITY F EXCEPT FOR OC OCTOBER 15.	OD OF JULY THE REPORTED THAT CTOBER 1 TO 0	ROUGH SEPTEMB .0 .0 .0 .0 UNIT 2 WAS D CTOBER 3. AN .0 .0	SER, 1983. DOWN THE ENTI	744 RE MON ANCE A 720	47 ITH OF (IND REP)	O OCTOBER AIR BEG O	1.0 SAN ON .0
	203 SYSTEM ** PROB 202 203 SYSTEM	100.0 100.0 BLEMS/SOLUTI	FOR THE PERIO .0 .0 .0 IONS/COMMENTS THE UTILITY F EXCEPT FOR OC OCTOBER 15.	OD OF JULY THE REPORTED THAT CTOBER 1 TO 0	ROUGH SEPTEMB .0 .0 .0 .0 UNIT 2 WAS D CTOBER 3. AN .0	SER, 1983. DOWN THE ENTI	744 RE MON ANCE A 720	47 ITH OF (IND REP)	O OCTOBER AIR BEG O	1.0 SAN ON .0
1/83	203 SYSTEM ** PROB 202 203 SYSTEM ** PROB	100.0 100.0 BLEMS/SOLUTI	FOR THE PERIO .0 .0 CONS/COMMENTS THE UTILITY F EXCEPT FOR OC OCTOBER 15. CONS/COMMENTS UNIT 2 WAS DO	OD OF JULY THE REPORTED THAT CTOBER 1 TO 0	ROUGH SEPTEMB .0 .0 .0 .0 UNIT 2 WAS D CTOBER 3. AN .0 .0 .0	SER, 1983. DOWN THE ENTI	744 RE MON ANCE A 720	47 ITH OF (IND REP)	O OCTOBER AIR BEG O	1.0 SAN ON .0
1/83	203 SYSTEM ** PROB 202 203 SYSTEM ** PROB	100.0 100.0 3LEMS/SOLUTI	FOR THE PERIO .0 .0 CONS/COMMENTS THE UTILITY F EXCEPT FOR OC OCTOBER 15. CONS/COMMENTS UNIT 2 WAS DO	OD OF JULY THE REPORTED THAT CTOBER 1 TO 0	ROUGH SEPTEMB .0 .0 .0 .0 UNIT 2 WAS D CTOBER 3. AN .0 .0 .0 .0	SER, 1983. DOWN THE ENTI	744 RE MON ANCE A 720	47 ITH OF (IND REP)	O OCTOBER AIR BEG O	1.0 GAN ON .0
1/83	203 SYSTEM ** PROB 202 203 SYSTEM ** PROB	100.0 100.0 BLEMS/SOLUTI	FOR THE PERIOR .0 .0 .0 CONS/COMMENTS THE UTILITY FOR OCCOMMENTS OCTOBER 15. CONS/COMMENTS UNIT 2 WAS DORED REPAIR.	OD OF JULY THE REPORTED THAT CTOBER 1 TO 0	ROUGH SEPTEMB .0 .0 .0 .0 UNIT 2 WAS D CTOBER 3. AN .0 .0 .0	SER, 1983. DOWN THE ENTI	744 RE MON ANCE A 720	47 ITH OF (IND REP)	O OCTOBER AIR BEG O	1.0 SAN ON .0
	203 SYSTEM ** PROB 202 203 SYSTEM ** PROB	100.0 100.0 BLEMS/SOLUTI	FOR THE PERIO .0 .0 .0 CONS/COMMENTS THE UTILITY FOR OCCOMMENTS CONS/COMMENTS UNIT 2 WAS DORED TO THE PAIR.	DE OF JULY THE	ROUGH SEPTEMB .0 .0 .0 .0 UNIT 2 WAS D CTOBER 3. AN .0 .0 .0 .0 .0 .0	OOWN THE ENTI NUAL MAINTEN	744 RE MONIANCE A 720 NNUAL	47 ATH OF C AND REPA O MAINTEN	O DCTOBER AIR BEG O NANCE A	1.0 SAN ON .0
1/83	203 SYSTEM ** PROB 202 203 SYSTEM ** PROB	100.0 100.0 BLEMS/SOLUTI	FOR THE PERIO .0 .0 .0 CONS/COMMENTS THE UTILITY FOR OCCOMMENTS CONS/COMMENTS UNIT 2 WAS DORED TO THE PAIR.	DE OF JULY THE REPORTED THAT CHOSER 1 TO O	ROUGH SEPTEMB .0 .0 .0 .0 UNIT 2 WAS D CTOBER 3. AN .0 .0 .0 .0	OWN THE ENTITION OF THE ENTITY	744 RE MONANCE A 720 NNUAL	47 ITH OF (IND REP) O MAINTEN	O DCTOBER AIR BEG O NANCE A	1.0 SAN ON .0
1/83 2/83	203 SYSTEM ** PROB 202 203 SYSTEM ** PROB	100.0 100.0 BLEMS/SOLUTI	FOR THE PERIO .0 .0 .0 CONS/COMMENTS THE UTILITY FOR OCCOMMENTS CONS/COMMENTS UNIT 2 WAS DORED TO THE PAIR.	DE OF JULY THE REPORTED THAT CHOSER 1 TO O	ROUGH SEPTEMB .0 .0 .0 .0 UNIT 2 WAS D CTOBER 3. AN .0 .0 .0 .0 .0 .0 .0 .0 .0 .0 .0 .0 .0	OWN THE ENTITION OF THE ENTITY	744 RE MONANCE A 720 NNUAL	47 ITH OF (IND REP) O MAINTEN	O DCTOBER AIR BEG O NANCE A	1.0 SAN ON .0
1/83	203 SYSTEM ** PROB 202 203 SYSTEM ** PROB 202 203 SYSTEM ** PROB	100.0 100.0 3LEMS/SOLUTI 100.0 100.0 100.0 100.0 100.0 100.0	FOR THE PERIO .0 .0 .0 CONS/COMMENTS THE UTILITY FOR OCCOMMENTS CONS/COMMENTS UNIT 2 WAS DORED TO THE PAIR.	DE OF JULY THE REPORTED THAT CHOSER 1 TO O	ROUGH SEPTEMB .0 .0 .0 .0 UNIT 2 WAS D CTOBER 3. AN .0 .0 .0 .0 .0 .0 .0 .0 .0 .0 .0 .0 .0	OWN THE ENTITION OF THE ENTITY	744 RE MONANCE A 720 NNUAL	47 ITH OF (IND REP) O MAINTEN	O DCTOBER AIR BEG O NANCE A	1.0 SAN ON .0

PERIOD	MODULE	AVAILABILITY	OPERABILITY		UTILIZATION	SO2 PART.	HOURS	HOURS		
•	** PRO	BLEMS/SOLUTIO	NS/COMMENTS							
		,	NNUAL MAINTE	NAME AND DE	DATES MEDE CO	OMBLETED ON	DECEMBE	D 16	THE UN	AM TTE
		•	MINOAL HAINTE	NANCE AND RE	FAIRS MERE C	ONFLETED ON	DECEMBE	K 14.	1112 01	111 845
2/84	-	100.0			.0					
	203	100.0			.0				_	_
	SYSTEM	100.0			.0		696	0	0	. 0
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
		ŧ	JNIT 2 WAS OF	F LINE DURIN	G JANUARY AN	D FEBRUARY D	UE TO L	OW POW	ER DEMA	AND.
3/84	202	100.0	. 0		.0					
J. J.	203		27.1	89.5	5.8					
	SYSTEM	100.0	27.1	89.5	5.8		744	158	43	8.3
6.786	202	100 0	40.9	100 0	77 7					
47.04	203	35.5	43.6	100.0	35.5					
	SYSTEM	100.0	84.5	100.0	68.8		720	587	496	40.4
	0.0.2	200.0	01.5	200.0	33.3		, 20	30,	.,0	
5/84	202	100.0	39.9 60.1	100.0	39.9					
	203	98.8	60.1	98.0	60.1					
	SYSTEM	100.0	100.0	100.0	100.0		744	744	744	73.0
6/84	202	99.6	6.5	100.0	5.0					
	203	98.8	98.1	100.0	74.6					
	SYSTEM	100.0	100.0	100.0	79.6		720	548	573	46.5
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS							
			THE UTILITY R	_			OBLEMS	WERE E	NCOUNTE	ERED
7/84	202	88.2	87 3	87.6	79.9					
,, 01	203	.0	.0	07.0	.0					
		44.1		87.6			744	682	297	60.2
	** PRO	BLEMS/SOLUTION	ONS/COMMENTS							
			MAINTENANCE WOOD JULY 4, 19		ON MODULE 2	AW TI DNA SO	S PLACE	D BACK	інто :	SERVICE
		1	MODULE 203 WA	S OUT OF SER	VICE DURING	THE ENTIRE M	юнтн оғ	JULY.		
8/84	SYSTEM						744			
9/84	SYSTEM						720			
// UT	212111						120			

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR AUGUST AND SEPTEMBER 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

ARIZONA ELECTRIC POWER COMPANY NAME PLANT NAME UNIT NUMBER 3 COCHISE CITY ARIZONA STATE REGULATORY CLASSIFICATION 43. (.100 LB/MMBTU)
344. (.800 LB/MMBTU)
301. (.700 LB/MMBTU)
530
195 PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW NET UNIT GENERATING CAPACITY W/FGD - MW 175 183 NET UNIT GENERATING CAPACITY WO/FGD - MW EQUIVALENT SCRUBBED CAPACITY - MW 98 ** UNIT DATA - BOILER AND STACK RILEY STOKER BOILER SUPPLIER BOILER TYPE PULVERIZED COAL BOILER SERVICE LOAD BASE DESIGN BOILER FLUE GAS FLOW - CU.M/S
BOILER FLUE GAS TEMPERATURE - C
STACK HEIGHT - M 520.98 (1104000 ACFM) 376.7 (710 F) 122. (400 FT) CONCRETE 4.9 (16.2 FT) STACK SHELL STACK TOP DIAMETER - M ** FUEL DATA FUEL TYPE COAL FUEL GRADE SUBBITUMINOUS 23260. (10000 BTU/LB) AVERAGE HEAT CONTENT - J/G 15.00 RANGE HEAT CONTENT BTU/LB 9500-10800 AVERAGE ASH CONTENT - % 15-20 13.00 9.0-15.0 RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - % RANGE MOISTURE CONTENT - % AVERAGE SULFUR CONTENT - % . 70 RANGE SULFUR CONTENT - %
AVERAGE CHLORIDE CONTENT % 0.4-0.6 .01 0.00-0.03 RANGE CHLORIDE CONTENT - % *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER 0 TYPE NONE ** ESP NUMBER NUMBER OF SPARES TYPE HOT SIDE SUPPLIER

SUPPLIER

INLET FLUE GAS CAPACITY - CU.M/S

INLET FLUE GAS TEMPERATURE - C

PRESSURE DROP - KPA

PADTICIF REMOVAL EFFICENCY - %

AIR CORRECTION DIVISION, OUR
(1104000 ACFM)

710 F)

1 (1. IN-H20)

710 F)

710 F) ** PARTICLE SCRUBBER NUMBER GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL LINER GENERIC MATERIAL N/A LINER SPECIFIC MATERIAL N/A GAS CONTACTING DEVICE TYPE N/A

13-42

*** FGD SYSTEM

```
** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                               THROWAWAY PRODUCT
   SO2 REMOVAL MODE
                                               WET SCRUBBING
   PROCESS TYPE
                                              LIMESTONE
   PROCESS ADDITIVES
                                               NONE
                                               RESEARCH-COTTRELL
   SYSTEM SUPPLIER
                                               BURNS & MCDONNELL
   A-E FIRM
   DEVELOPMENT LEVEL
                                               FULL SCALE
   NEW/RETROFIT
                                               NFW
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.60
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                 85.00
   ENERGY CONSUMPTION - %
                                                   4.1
   CURRENT STATUS
                                                6/79
    COMMERCIAL START-UP
   INITIAL START-UP
CONTRACT AWARDED
                                                6/79
                                                8/74
** DESIGN AND OPERATING PARAMETERS
    DESIGN COAL SULFER CONTENT - %
                                                   1.00
                                                              ( 10000 BTU/LB)
    DESIGN COAL HEAT CONTENT - J/G
                                               23260.0
    DESIGN COAL ASH CONTENT - %
                                                17.00
    DESIGN MOISTURE CONTENT - %
                                                 18.00
    DESIGN CHLORIDE CONTENT %
                                                   .00
                                                             ( 43560 SQ FT)
    SPACE REQUIREMENTS - SQ M
                                                4046.7
    OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                72.0
** QUENCHER/PRESATURATOR
    NUMBER
    TYPE
                                               CYCLONIC SPRAY QUENCHER
    SUPPLIER
                                               RESEARCH-COTTRELL
    INLET GAS FLOW - CU. M/S
                                                 188.76 ( 400000 ACFM)
    INLET GAS TEMPERATURE - C
                                                 132.2
                                                             ( 270 F)
    PRESSURE DROP - KPA
                                                             ( 1.0 IN-H20)
                                                   . 2
    LIQUID RECIRCULATION RATE - LITERS/S
                                                567.
                                                             ( 9000 GPM)
    L/G RATIO L/CU. M
                                                             ( 20.0 GAL/1000 ACFM)
                                                  2.7
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              AISI 1110
** ABSORBER
    NUMBER
                                                2
    NUMBER OF SPARES
                                                1
    GENERIC TYPE
                                               COMBINATION TOWER
                                               SPRAY/PACKED
    SPECIFIC TYPE
    TRADE NAME/COMMON TYPE
                                               N/A
                                               RESEARCH-COTTRELL
    SUPPLIER.
    DIMENSIONS - FT
                                               30.0 DIA X 110.0
    SHELL GENERIC MATERIAL
                                               CARBON STEEL
    SHELL SPECIFIC MATERIAL
                                               AISI 1110
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                               N/A
    LINER GENERIC MATERIAL
                                               ORGANIC
    LINER SPECIFIC MATERIAL
                                               GLASS FLAKE-FILLED POLYESTER
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                               FLAKELINE 103
    GAS CONTACTING DEVICE TYPE
                                               SPRAY ZONE & VERTICAL CROSS CHANNEL FIXED GRID P
    NUMBER OF CONTACTING ZONES
    LIQUID RECIRCULATION RATE LITER/S
                                                567.
                                                              ( 9000 GPM)
                                                              ( 40.0 GAL/1000 ACF)
    L/G RATIO - L/CU.M
                                                  5.3
    GAS-SIDE PRESSURE DROP KPA
                                                   .6
                                                              ( 2.5 IN-H20)
    SUPERFICAL GAS VELOCITY - M/SEC
                                                              ( 10.0 FT/S)
                                                   3.0
    INLET GAS FLOW - CU. M/S
                                                  94.38
                                                              ( 200000 ACFM)
    INLET GAS TEMPERATURE - C
                                                  68.3
                                                              ( 155 F)
    SO2 REMOVAL EFFICIENCY - %
                                                  97.0
    PARTICLE REMOVAL EFFICENCY - %
                                                  99.6
** MIST ELIMINATOR
    PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                               PRIMARY COLLECTOR
    NUMBER PER SYSTEM
                                                2
    NUMBER OF SPARES PER SYSTEM
                                                1
    NUMBER PER MODULE
    GENERIC TYPE
                                               IMPINGEMENT
    SPECIFIC TYPE
                                               BAFFLE
```

SPECIFIC TYPE

```
CLOSED VANE
   TRADE NAME/COMMON TYPE
   MANUFACTURER
                                               MUNTERS
                                               HORIZONTAL
   CONFIGURATION
   NUMBER OF STAGES
                                                   2
   NUMBER OF PASSES PER STAGE
   FREEBOARD DISTANCE M
                                                   .61
                                                             ( 2.0 FT)
   DISTANCE BETHEEN STAGES - CM
                                                  30.48
                                                              (12.0 IN)
                                                  10.2
   DISTANCE BETWEEN VANES CM
                                                              ( 4.00 IN)
   VANE ANGLES DEGREES
   PRESSURE DROP - KPA
                                                              ( 1.0 IN-H20)
                                                   ٠2
                                                              ( 10.0 FT/S)
   SUPERFICAL GAS VELOCITY - M/S
                                                   3.0
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              ORGANIC
                                               POLYVINYL CHLORIDE
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               FRESH
   WASH WATER SOURCE
                                              INTERMITTENT [LOWER STAGE]; ONCE EVERY HOUR [UPP
   WASH FREQUENCY
                                                             ( 200 GAL/MIN)
   WASH RATE - L/S
                                                 12.6
** REHEATER
                                                0
   NUMBER
                                               NONE
   GENERIC TYPE
   SPECIFIC TYPE
                                               N/A
    TRADE NAME/COMMON TYPE
                                               N/A
    PERCENT GAS BYPASSED - AVG
                                                  50.0
    TEMPERATURE INCREASE - C
                                                                 78 F)
                                                  43.3
                                                              ſ
   INLET FLUE GAS TEMPERATURE - C
                                                  46.1
                                                              ( 115 F)
    OUTLET FLUE GAS TEMPERATURE - C
                                                  89.4
                                                              ( 193 F)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               NONE
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              N/A
** FANS
   NUMBER
                                                2
   NUMBER OF SPARES
                                                0
                                               CENTRIFUGAL
   DESTGN
    SUPPLIER
                                               WESTINGHOUSE
   FUNCTION
                                               UNIT
    APPLICATION
                                               FORCED DRAFT
   SERVICE
                                               DRY
    FLUE GAS FLOW RATE CU.M/S
                                                 188.76
                                                              ( 400000 ACFM)
   FLUE GAS TEMPERATURE C
                                                              ( 270 F)
                                                 132.2
   PRESSURE DROP - KPA
                                                  6.2
                                                             (20.5 IN-H20)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              CARBON STEEL
** DAMPERS
   NUMBER
    FUNCTION
                                               SHUT-OFF
   GENERIC TYPE
                                               LOUVER
    SPECIFIC TYPE
                                               PARALLEL BLADE MULTILOUVER
   MODULATION
                                               OPEN/CLOSED
    SEAL AIR FLOW - CU. M/S
                                                    . 24
                                                                   500 ACFM)
                                                              •
   CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              NR
    LINER GENERIC MATERIAL TYPE
                                              NONE
   LINER SPECIFIC MATERIAL TYPE
                                               N/A
** DAMPERS
   NUMBER
                                               2
   FUNCTION
                                               SHUT-OFF
   GENERIC TYPE
                                               GUILLOTINE
   SPECIFIC TYPE
                                               TOP-ENTRY GUILLOTINE
   MODULATION
                                               OPEN/CLOSED
   SEAL AIR FLOW CU. M/S
                                                   . 24
                                                              1
                                                                 500 ACFM)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               ИR
    LINER GENERIC MATERIAL TYPE
                                               HIGH ALLOY
   LINER SPECIFIC MATERIAL TYPE
                                               NICKEL BASE/CHROMIUM-IRON-COPPER-MOLYBDENUM
** DAMPERS
   NUMBER
                                               2
   FUNCTION
                                               SHUT-OFF
   GENERIC TYPE
                                               LOUVER
```

PARALLEL BLADE MULTILOUVER

** DISPOSAL NATURE

TYPE

LOCATION

SITE TRANSPORTATION METHOD

MODULATION OPEN/CLOSED SEAL AIR FLOW - CU. M/S 500 ACFM) (.24 CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL CONSTRUCTION MATERIAL SPECIFIC TYPE NR LINER GENERIC MATERIAL TYPE HIGH ALLOY NICKEL BASE/CHROMIUM-IRON-COPPER-MOLYBDENUM LINER SPECIFIC MATERIAL TYPE ** DUCTWORK ABSORBER INLET LOCATION CONFIGURATION RECTANGULAR **DIMENSIONS** 12.0 X 14.0 SHELL GENERIC MATERIAL TYPE CARBON STEEL SHELL SPECIFIC MATERIAL TYPE AISI 1110 LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DUCTWORK ABSORBER OUTLET LOCATION CONFIGURATION RECTANGULAR 12.0 X 14.0 DIMENSIONS SHELL GENERIC MATERIAL TYPE CARBON STEEL SHELL SPECIFIC MATERIAL TYPE AISI 1110 LINER GENERIC MATERIAL TYPE ORGANIC FLUOROELASTOMER LINER SPECIFIC MATERIAL TYPE ** REAGENT PREPARATION EQUIPMENT FUNCTION WET BALL MILL COMPARTMENTED DEVICE DEVICE TYPE NR MANUFACTURER KENNEDY VAN SAUN NUMBER 1 NUMBER OF SPARES 0 FULL LOAD DRY FEED CAPACITY - M.TONS/HR 4.5 5 TPH) (PRODUCT QUALITY - % SOLIDS 45.0 ** TANKS SERVICE NUMBER ____ ABSORBER FEED 1 REAGENT FEED 1 MILL SLURRY SUMP 1 WASTE SLURRY SUMP 1 ** PUMPS SERVICE NUMBER ____ ABSORBER 3 QUENCHER 4 MILL SLURRY RECYCLE 2 ADDITIVE FEED 2 WASTE SLURRY TRANSFER 1 ** SOLIDS CONCENTRATING/DEWATERING DEVICE NONE *** SLUDGE MOISTURE CONTENT - % TOTAL FREE WATER 70.0 % CASO4 DRY 80.0 ** TREATMENT COHTAM NONE DEVICE N/A PROPRIETARY PROCESS N/A

FINAL

OFF-SITE

PIPELINE

POND

ARIZONA ELECTRIC POWER: APACHE 3 (CONT.)

SITE TREATMENT NONE

SITE DIMENSIONS
25 TO 30 ACRES BY 18 FT DEEP
SITE CAPACITY CU.M 611500 (500.0 ACRE-FT)

SITE SERVICE LIFE - YRS

** PROCESS CONTROL AND INSTRUMENTATION

PROCESS STREAM QUENCHER RECYCLE LINE
CHEMICAL PARAMETERS PH
PHYSICAL VARIABLES PERCENT SOLIDS
CONTROL LEVELS 5.0 PH
PROCESS CONTROL MANNER

PROCESS CONTROL MANNER MANUAL
PROCESS CHEMISTRY MODE FEEDBACK

** WATER BALANCE

WATER LOOP TYPE OPEN

MAKEUP WATER ADDITION - LITERS/S 115.9 (1840 GPM)

SOURCE OF MAKEUP WATER WELL WATER

** CHEMICALS AND CONSUMPTION

FUNCTION ABSORBENT
NAME LIMESTONE
PRINCIPAL CONSTITUENT >93% CACO3
SOURCE/SUPPLIER PAUL LIME
UTILIZATION % 99.0
POINT OF ADDITION BALL MILL

** FGD SPARE CAPACITY INDICES

ABSORBER % 100.0
MIST ELIMINATOR - % .0
FAN % .0
BALL MILL % .0
EFFLUENT HOLD TANK - % .0
RECIRCULATION PUMP % 50.0

** FGD SPARE COMPONENT INDICES

ABSORBER 1.0
MIST ELIMINATOR .0
FAN .0
BALL MILL .0
EFFLUENT HOLD TANK .0
RECIRCULATION PUMP 1.0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

6/79 SYSTEM 50.00 99.50 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE APACHE 3 BOILER AND FGD SYSTEM BEGAN OPERATIONS DURING JUNE. THE UTILITY REPORTED THAT THE START-UP WAS TYPICAL WITH NUMEROUS MINOR SHAKEDOWN PROBLEMS.

7/79 SYSTEM 744

8/79 SYSTEM **744**

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT EXTENSIVE PROBLEMS WITH THE REAGENT HANDLING SYSTEM ARE CONTINUING PARTICULARLY WITH RESPECT TO FEED LINE FAILURES, PIPING PLUGGING AND GRINDING OPERATIONS. THE REAGENT HANDLING SYSTEM ACCOMODATES BOTH UNITS 2 AND 3.

9/79 SYSTEM 720

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS FACTOR ** PROBLEMS/SOLUTIONS/COMMENTS DURING THE THIRD QUARTER OF 1979 THE BOILER AND FGD SYSTEM ONLY OPERATED ABOUT 25% OF THE TIME BECAUSE OF CONTINUING PROBLEMS WITH THE REAGENT FEED LINE. THE FRP SECTION FROM THE GRINDER TO THE SCRUBBERS FAILED. THE LINE WAS REPAIRED AT THE END OF SEPTEMBER. COMMERCIAL OPERATIONS AT APACHE 3 BEGAN ON SEPTEMBER 1. 10/79 SYSTEM .0 . 0 744 ٥ . 0 ** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY IS IN THE PROCESS OF REPLACING THE REAGENT HANDLING SYSTEM; THEREFORE, THE FGD SYSTEM DID NOT OPERATE DURING OCTOBER. 11/79 302 89.4 39.8 39.4 39.4 303 89.4 50.5 50.0 50.0 SYSTEM 100.0 90.3 89.4 89.4 720 713 644 92.7 12/79 SYSTEM 99.5 99.5 99.5 99.5 744 744 741 95.4 ** PROBLEMS/SOLUTIONS/COMMENTS THE REAGENT HANDLING SYSTEM REPLACEMENT WAS COMPLETED IN DECEMBER. THE OUTAGE TIME DURING DECEMBER WAS CAUSED BY A FAULTY BOILER FLUE DAMPER. 1/80 SYSTEM 91.7 91.7 91.7 91.7 744 744 682 89.7

** PROBLEMS/SOLUTIONS/COMMENTS

DURING JANUARY SOME OUTAGE TIME WAS DUE TO A PUMP MALFUNCTION.

OUTAGE TIME WAS ALSO CAUSED BY A BROKEN FEED BELT TO THE LIMESTONE BALL MILL.

2/80 SYSTEM 95.6 74.1 96.0 71.4 696 671 497 83.5

** PROBLEMS/SOLUTIONS/COMMENTS

DURING FEBRUARY OUTAGE TIME RESULTED FROM AN ESP FAILURE.

FORCED OUTAGE TIME WAS ALSO CAUSED BY A PUMP MALFUNCTION.

3/80 SYSTEM 90.9 90.9 90.9 90.9 744 744 677 91.1

** PROBLEMS/SOLUTIONS/COMMENTS

SOME OF THE OUTAGE TIME DURING MARCH OCCURRED BECAUSE OF PUMP FAILURES.

OUTAGE TIME RESULTED FROM STICKING VALVES AND LIMESTONE FEED-BELT PROBLEMS.

PROBLEMS

4/80 SYSTEM 99.0 96.9 96.9 30.6 720 227 220

** PROBLEMS/SOLUTIONS/COMMENTS

DURING APRIL THE FGD SYSTEM WAS FORCED DOWN DUE TO PUMP FAILURES AND A RUPTURE IN THE SLURRY RECIRCULATION LINE.

5/80 SYSTEM .0 .0 .0 .744 39 0

ARIZONA ELECTRIC POWER: APACHE 3 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER AND FGD SYSTEM WERE DOWN FOR A SCHEDULED OVERHAUL. THE LINERS IN THE ABSORBER QUENCHER HAD TO BE REPAIRED. THE BOILER RETURNED TO SERVICE BEFORE REPAIR WORK FOR THE FGD SYSTEM WAS COMPLETE. THE FGD SYSTEM WAS UNAVAILABLE IN MAY BECAUSE OF THIS OVERHAUL.

6/80 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE DATA FOR THE MONTH OF JUNE HAS BEEN MISPLACED.

7/80	302	29.0	30.0	90.0	29.0				
	303	.0	.0		.0				
	SYSTEM	29.0	30.0	90.0	29.0	744	721	216	49.3

** PROBLEMS/SOLUTIONS/COMMENTS

BOTH MODULES WERE UNAVAILABLE BECAUSE OF REPLACEMENT OF THE ABSORBER LINER. MODULE 302 WAS OUT OF SERVICE FOR 22 DAYS, WHILE MODULE 303 WAS OUT OF SERVICE DURING ALL OF JULY.

A PACKING PUMP FAILURE CAUSED THE FGD SYSTEM TO GO DOWN.

8/80	302	98.5	47.8	96.3	38.4				
	303	98.5	19.3	91.3	15.5				
	SYSTEM	98.5	67.1	94.8	54.0	744	599	402	41.5

** PROBLEMS/SOLUTIONS/COMMENTS

TOWER 302 WAS UNAVAILABLE DURING PART OF AUGUST BECAUSE OF A QUENCHER PUMP FAILURE.

DUE TO A SAMPLING LINE FAILURE IN AUGUST, TOWER 303 WAS SHUT DOWN FOR PART OF THE MONTH.

THE REDUCED RATE OF FGD OPERATION IN AUGUST WAS A RESULT OF BOILER UNIT PROBLEMS AND REDUCED LOAD CAPACITY.

9/80 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

NO INFORMATION WAS AVAILABLE FOR SEPTEMBER 1980.

10/80	302	76.2	87.7	97.1	68.1			
		.0	.0		.0			
	SYSTEM	76.2	87.7	97.1	68.1	744	567	507 52.5

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER WAS OPERATED AT A REDUCED LOAD FOR 60 HOURS AND WAS TAKEN OFF LINE FOR SIX DAYS DURING OCTOBER.

UNAVAILABLE FGD SYSTEM TIME WAS DUE TO A QUENCHER PUMP FAILURE AND PH INSTABILITY.

11/80	302	78.4	78.1	95.4	77.8				
	303	100.0	17.8	100.0	17.8				
	SYSTEM	100.0	96.0	100.0	95.6	7,,			
			,0.0	100.0	73.0	744	717	688 99	1.6

744

720

342

258 44.5

729

719 86.2

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

DURING NOVEMBER THE FGD SYSTEM WAS FORCED OUT OF SERVICE DUE TO FAILURE OF THE QUENCHER PUMPS, SAMPLE LINE AND TRANSFORMER.

THE BOILER UNIT TRIPPED CAUSING APPROXIMATELY FIVE HOURS OF OUTAGE TIME DURING THE MONTH.

12/80 302 .0 .0 .0 .0 .0 303 100.0 98.6 100.0 96.6 SYSTEM 100.0 98.6 100.0 96.6

** PROBLEMS/SOLUTIONS/COMMENTS

NO FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE MONTH OF DECEMBER.

1/81 302 . 0 . 0 . 0 303 100.0 52.9 100.0 46.1 SYSTEM 100.0 52.9 100.0 46.1 744 649 343 80.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER WAS OUT OF SERVICE APPROXIMATELY 123 HOURS DURING JANUARY.

MODULE 303 WAS TAKEN OUT OF SERVICE FOR APPROXIMATELY 272 HOURS DUE TO THE LOW SULFUR CONTENT OF THE COAL. MODULE 302 WAS NOT AVAILABLE FOR OPERATION DURING JANUARY.

2/81 302 .0 .0 .0 303 100.0 27.4 100.0 27.4 SYSTEM 100.0 27.4 100.0 27.4

27.4 100.0 27.4 672 672 184 95.6

** PROBLEMS/SOLUTIONS/COMMENTS

DURING FEBRUARY THE OPERATION OF THE FGD SYSTEM WAS REDUCED DUE TO THE LOW SULFUR CONTENT OF THE COAL.

REPAIRS WERE MADE ON TOWER 302 DURING THE MONTH.

3/81 302 78.5 23.7 52.5 23.7 303 .0 .0 .0 .0 SYSTEM 78.5 23.7 52.5 23.7

23.7 52.5 23.7 744 744 177 87.5

** PROBLEMS/SOLUTIONS/COMMENTS

DURING MARCH LOW OPERABILITY OF MODULE 302 WAS DUE TO THE FIRING OF LOW SULFUR COAL.

MODULE 303 WAS UNAVAILABLE DUE TO A MALFUNCTION OF THE LIMESTONE GRINDING CIRCUIT.

4/81 302 100.0 75.3 100.0 35.8 303 .0 .0 .0 .0 SYSTEM 100.0 75.3 100.0 35.8

** PROBLEMS/SOLUTIONS/COMMENTS

DURING APRIL THE BOILER WAS UNAVAILABLE DUE TO A 2 WEEK SCHEDULED MAINTENANCE OUTAGE.

MODULE 303 WAS NOT AVAILABLE FOR OPERATION DUE TO ERROSION PROBLEMS DISCOVERED IN THE MODULE BOWL AREA. THIS HAS BEEN A CONTINUAL PROBLEM AND THE UTILITY IS PRESENTLY CONDUCTING STUDIES TO ALLEVIATE THE PROBLEM.

					NCE DATA (UTILIZATION	% REN	10VAL	PER		FGD	
5/81	302	100.0	87.1	100.0	87.1						
3/01	303	100.0		100.0	.0						
		100.0		100.0				744	648	648	90.0
	** PROE	BLEMS/SOLUTI	ONS/COMMENTS								
			DURING MAY THI TO MAINTENANCI		TAKEN OUT OF	SERVI	CE AP	PROXIM	ATELY 9	6 HOURS	5 DUE
6/81		100.0	86.7	100.0	86.7						
	303 SYSTEM	100.0 100. 0	.0 86.7	100.0	.0 86.7			720	720	624	87.1
	** PROE	BLEMS/SOLUTI	ONS/COMMENTS								
			DURING JUNE M	DDULE 303 WA	S OUT OF SERV	ICE DU	JE TO I	REPAIRS	S ON THE	E ESP.	
7/81		45.2	11.9	100.0	10.8						
	303 SYSTEM	100.0 100.0	57.3	100.0	51.6			7//			
				100.0	69.2			744	6/0	464	77.6
	** PROE		ONS/COMMENTS								
			MITH THE ELEC.	TROSTATIC PR	OM SERVICE ON ECIPITATOR. TIVE MAINTENA	MODULE	303	WAS PLA	ACED IN	SERVIC	E
8/81	302	. 0	. 0		. 0						
			100.0	100.0	100.0						
	SYSTEM	100.0	100.0	100.0	100.0			744	744	744	89.1
9/81	302	.0	.0		.0						
		62.4 62.4		62.4 62.4	62.4 62.4			720	718	440	80.8
			ONS/COMMENTS		02.1			720	710	447	60. 6
			AS A RESULT OF CLOSE.	F A MALFUNCT	OR APPROXIMAT	ELY EL ED THE	EVEN (DAYS DU F AND (TRING SE	PTEMBE AMPERS	R 5 TO
10/81		.0	. 0		.0						
	303 SYSTEM	96.2 96.2	98.2 98.2	96.2	96.2						
		_	ONS/COMMENTS	96.2	96.2			744	729	716	78.6
			DURING OCTOBER QUENCHER PUMPS	TOWER 303	WAS OUT OF SE	RVICE	FOR T	HREE HO	OURS TO	CHANGE	THE
			ADDITIONAL FG	SYSTEM OUT	AGE TIME RESU	LTED F	ROM U	VIT TR	IPS.		
11/81	302	.0	.0		88.1						
	303 SYSTEM	100.0 100.0	100.0 100.0	88.1 88.1	88.1 88.1			720	634	670	63.6
	** PROS	BLEMS/SOLUTI	ONS/COMMENTS		- 3.2			, 20	0.54	034	03.0
			MODULE 303 WAS	OUT OF SER	VICE FROM NOV	EMBER	3 THRO	DUGH NO	OVEMBER	11 DUE	то
2/81	SYSTEM							744			
								/44			

	302 303 SYSTEM	95.1 95.1	TONS/COMMENTS THE ORIGINAL C 84.0 0 84.0 TONS/COMMENTS DURING JANUARY LEAK IN THE CO	93.7	73.2 .0	TE INFORM				MAIL.
	303 SYSTEM ** PRO	95.1	84.0 .0 84.0 TONS/COMMENTS	93.7	73.2 .0	TE INFORMA				MAIL.
	303 SYSTEM ** PRO	95.1	.0 84.0 CIONS/COMMENTS YAAUNAK JANUARY		۰.0		7 44			
2/82	SYSTEM ** PRO	95.1	84.0 CIONS/COMMENTS TANUARY JANUARY	93.7	73.2		744			
2/82		BLEMS/SOLUT	DURING JANUARY				, , , ,	648	544	62.2
2/82	302									
2/82	302							TIME	DUE TO	A
		95.5	93.9	95.5	93.6					
	303 SYSTEM	95.5	.0 93.9	95.5	.0 93.6		672	670	635	84.4
	** PROI	BLEMS/SOLUT	IONS/COMMENTS							
			DURING FEBRUAR MAINTENANCE ON			OF OUTAGE	E TIME WA	S REQU	IRED FO)R
3/82	302	21.9	24.6	20.6	20.3					
	303 SYSTEM	.0 21.9	.0 24.6	20.6	.0 20.3		744	615	151	47.2
	** PRO	BLEMS/SOLUT	TIONS/COMMENTS							
			ON MARCH 6, BO RECONSTRUCTION FOR THE REMAIN	. THIS RESU	LTED IN SUSF					UND
4/82	302	.0	.0		.0					
	303 SYSTEM	.0			. 0 . 0		720	53	0	3.8
	** PROBLEMS/SOLUTIONS/COMMENTS									
			ON APRIL 1 AND		TH MODULES #	IERE OUT OF	F SERVICE	FOR M	AJOR RE	PAIR
			AS OF APRIL 3,	THE UNIT WA	S DOWN FOR A	MNUAL MAIN	TENANCE	AND RE	PAIR.	
5/82	302	.0	.0		.0					
	303 SYSTEM	.0	. 0 .0		. 0 . 0		744	510	0	49.6
	** PRO	BLEMS/SOLUT	IONS/COMMENTS							
			THE FGD SYSTEM		SERVICE FOR	THE MONTH	OF MAY F	FOR MAJ	OR REPA	AIR
6/82	302 303	52.4	.0 49.2	45.0	.0 38.9					

** PROBLEMS/SOLUTIONS/COMMENTS

MODULE 303 WAS PLACED BACK IN SERVICE ON JUNE 11 AFTER COMPLETION OF MAJOR REPAIRS AND RECONSTRUCTION.

MODULE 303 WAS TAKEN OFF-LINE FOR APPROXIMATELY THREE DAYS DUE TO HIGH OPACITY AND A QUENCHER PUMP MALFUNCTION.

PERICO	MODULE A	VAILABILI	TY OPERABILITY	RELIABILITY	UTILIZATION	% REMOVAL SO2 PART.				
			ESP REPAIRS SH	THE SYSTE	M DOWN FOR	APPROXIMATEL'	THRE	E DAYS.		
7/82	302	59.0		100.0						
	303 System	40.9	41.3 97.9	100.0	40.9		766	738	722	07.0
			IONS/COMMENTS	100.0	77.0		/44	736	722	07.0
	AA PRODE	21137 30201	MODULE 303 WAS	S TAKEN OUT O	F SERVICE O	N JULY 13 TO	REPAIR	R A LEAR	IN TH	ΙE
			PACKING RETURN	I LINE TO THE	ABSORBER F	EED TANK.				
			MODULE 302 WAS REPAIRS AND RE			ULY 13 AFTER	COMPLE	TION OF	MAJOR	?
			MODULE 302 WAS PURPOSES.	OUT OF SERV	ICE APPROXI	MATELY 11 HOU	JRS ON	JULY 23	FOR T	ESTING
			MODULE 302 WAS	OUT OF SERV	ICE 11 HOUR	S ON JULY 26	DUE TO	A TRIE	OF UN	IIT 3.
8/82	302	96.8	95.3	96.4	87.6					
	30 3	100.0	. 0		.0					
	SYSTEM	96.8	95.3	96.4	87.6		744	685	652	85.9
	** PROBL	EMS/SOLUT	IONS/COMMENTS							
			THE UTILITY REDURING AUGUST.		NO MAJOR FGI	D-RELATED PRO	BLEMS	WERE EN	COUNTE	RED
9/82	302	100.0 100.0	85.3 .0	100.0	72.8					
	303 System	100.0	85.3	100.0	.0 72.8		720	615	524	60.8
	** PROBL	EMS/SOLUT	IONS/COMMENTS							
			THE UTILITY REDURING SEPTEME	PORTED THAT I	NO MAJOR FGI	D-RELATED PRO	BLEMS	WERE EN	ICOUNTE	RED
10/82	302	100.0	91.0	100.0	90.9					
	303	100.0	.0 91.0	•••	. 0					
	2121EU	100.0	91.0	100.0	90.9		744	743	676	74.6
	** PROBLEMS/SOLUTIONS/COMMENTS									
			THE UTILITY REDURING OCTOBER	PORTED THAT !	NO MAJOR FGI	D-RELATED PRO	BLEMS	WERE EN	COUNTE	RED
11/82		98.4	65.4	97.1	53.8					
	303 SYSTEM	100.0 98.4	.0 65.4	07.1	.0					
				97.1	53.8		720	592	387	55.3
	** PROBL	EMS/SOLUT	IONS/COMMENTS							
			THE UTILITY REDURING NOVEMBE	PORTED THAT I	NO MAJOR FGI	O-RELATED PRO	BLEMS	WERE EN	COUNTE	RED
2/02	302	100.0	69.2	100.0	61.6					
12/02				200.0	01.0					
12/02	303 SYSTEM	100.0 100.0	.0 69.2	100.0	.0					

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE REPORTED BY THE UTILITY DURING DECEMBER.

	MODULE AV	AILABILITY	OPERABILITY		NCE DATA UTILIZATION	% REI	10VAL	PER	BOILER HOURS		CAP.
1/83	302	8.1	5.8	100.0	4.8						
1, 00	303	78.6									
	SYSTEM	86.7	40.6	68.1 100.0	33.2			744	609	247	40.2
	** PROBLE	MS/SOLUTION	NS/COMMENTS								
			ODULE 302 WAS AN MALFUNCTIO		OF SERVICE ON	UMAL 1	ARY 3	DUE TO	AN IND	UCED DI	RAFT
		M	ODULE 303 WAS	PLACED BAC	K IN SERVICE	ON JAI	TUARY	6.			
2/83	302	100.0	. 0		.0						
	303	100.0	74.3	100.0	20.7						
	SYSTEM	100.0	74.3	100.0	20.7			672	187	139	17.5
	** PROBLE	MS/SOLUTIO	NS/COMMENTS								
		T	HE UNIT WAS T	AKEN OFF LI	NE FEBRUARY 8	B DUE	TO LOW	DEMAN	.		
3/83	302	100.0	17.6	100.0	10.7						
	303	100.0		100.0							
	SYSTEM	100.0	68.5	100.0	41.8			744	454	311	43.4
	** PROBLE	MS/SOLUTIO	NS/COMMENTS								
		Т	HE UNIT WAS O	FF LINE FRO	M MARCH 18 TO	MARC	H 28 D	UE TO	LOW DEM	AND.	
4/83					.0						
	303 System				.0			720	0	0	. 0
		EMS/SOLUTIO	NS/COMMENTS					, = 0	-	·	
			NIT 3 WAS DOW EPAIR.	N DURING TH	E MONTH OF AF	PRIL F	OR ANN	UAL MA	INTENAN	CE AND	
5/83	302				.0						
رن بر	303				.0						
	SYSTEM				.0			744	0	0	.0
		EMS/SOLUTIO	NS/COMMENTS					744	0	0	.0
			NS/COMMENTS NIT 3 WAS DOW	IN DURING MA	.0	MAINT	ENANCE			0	.0
6/83	** PROBLE	91.7	NIT 3 WAS DOW	IN DURING MA	.0 Y FOR ANNUAL 36.6	MAINT	ENANCE			0	.0
6/83	** PROBLE	U	NIT 3 WAS DOW		.0 Y FOR ANNUAL	MAINT	ENANCE		EPAIR.		.0
6/83	** PROBLE 302 303 SYSTEM	91.7 100.0 91.7	NIT 3 WAS DOW 42.2 .0	81.5	.0 Y FOR ANNUAL 36.6 .0	MAINT	ENANCE	AND R	EPAIR.		
6/83	** PROBLE 302 303 SYSTEM	91.7 100.0 91.7 EMS/SOLUTIO	NIT 3 WAS DOW 42.2 .0 42.2 NS/COMMENTS HE UTILITY RE	81.5 81.5	.0 Y FOR ANNUAL 36.6 .0 36.6			AND R	EPAIR. 624	263	50.8
	** PROBLE 302 303 SYSTEM ** PROBLE	91.7 100.0 91.7 EMS/SOLUTIO T 0	NIT 3 WAS DOW 42.2 .0 42.2 NS/COMMENTS HE UTILITY RE URING JUNE.	81.5 81.5 PORTED THAT	.0 Y FOR ANNUAL 36.6 .0 36.6 NO MAJOR FGE			AND R	EPAIR. 624	263	50.8
6/83	** PROBLE 302 303 SYSTEM ** PROBLE	91.7 100.0 91.7 EMS/SOLUTIO T 0	NIT 3 WAS DOW 42.2 .0 42.2 NS/COMMENTS HE UTILITY RE URING JUNE. 56.0	81.5 81.5	.0 Y FOR ANNUAL 36.6 .0 36.6 NO MAJOR FGE			AND R	EPAIR. 624	263	50.8
	** PROBLE 302 303 SYSTEM ** PROBLE	91.7 100.0 91.7 EMS/SOLUTIO T 0	NIT 3 WAS DOW 42.2 .0 42.2 NS/COMMENTS HE UTILITY RE URING JUNE.	81.5 81.5 PORTED THAT	.0 Y FOR ANNUAL 36.6 .0 36.6 NO MAJOR FGE			AND R	EPAIR. 624 WERE E	263 NCOUNT	50.8
7/83	** PROBLE 302 303 SYSTEM ** PROBLE 302 303 SYSTEM	91.7 100.0 91.7 EMS/SOLUTIO T 0 99.4 100.0 99.4	NIT 3 WAS DOW 42.2 .0 42.2 NS/COMMENTS HE UTILITY RE URING JUNE. 56.0 .0 56.0	81.5 81.5 PORTED THAT 97.7 97.7	.0 Y FOR ANNUAL 36.6 .0 36.6 NO MAJOR FGE 25.3 .0 25.3			AND RI 720 OBLEMS	EPAIR. 624 WERE E	263 NCOUNT	50.8 ERED
7/83	** PROBLE 302 303 SYSTEM ** PROBLE 302 303	91.7 100.0 91.7 EMS/SOLUTIO T 0 99.4 100.0	NIT 3 WAS DOW 42.2 .0 42.2 NS/COMMENTS HE UTILITY RE URING JUNE. 56.0 .0	81.5 81.5 PORTED THAT 97.7	.0 Y FOR ANNUAL 36.6 .0 36.6 NO MAJOR FGE 25.3			AND RI 720 OBLEMS	EPAIR. 624 WERE E	263 NCOUNT	50.8 ERED

ARIZONA ELECTRIC POWER: APACHE 3 (CONT.)

		VAILABILI			UTILIZATION	SO2 PART.	HOURS	HOURS	HOURS	FACTOR
	** PROBL	EMS/SOLUT	IONS/COMMENT	S						
				REPORTED THAT	NO MAJOR FGD	-RELATED PR	OBLEMS	WERE E	NCOUNTE	ERED
9/83	302				.0					
	303	100.0 100.0	.0		.0			_		_
					.0		/20	7	U	.1
	** PROBL	EMS/SOLUT	IONS/COMMENT	5						
			BOTH MODULE: AT REDUCED		SERVICE DURING	G SEPTEMBER	DUE TO	THE U	NIT OPE	RATING
10/83	302	100.0	.0 38.8		.0					
	303	98.5	38.8	95.9	35.2					
	SYSTEM	100.0	38.8	95.9	35.2		744	675	262	40.8
11/83	302	100.0 96.7	.0		. 0					
	303	96.7	.0 44.4	91.9	38.0					
	SYSTEM	100.0	44.4	91.9	38. 0		720	616	274	41.0
12/83	302	10 0.0 99.8	.0 21.6		.0					
					18.0					
	SYSTEM	100.0	21.6	98.9	18.0		744	618	134	29.2
	** PROBL	EMS/SOLUT	IONS/COMMENTS	5						
			NO MAJOR FGI	-RELATED PROB	LEMS WERE REPO	ORTED DURING	G THE F	ט אדא ט	QUARTER	OF
1/84		100.0			.0					
1/84	303	100.0	29.1	100.0	26.9					
1/84		100.0	29.1	100.0			744	690	201	35.7
	303 SYSTEM 302	100.0	29.1 29.1	100.0	26.9 26.9 .0		744	690	201	35.7
	303 SYSTEM 302 303	100.0 100.0 100.0 99.9	29.1 29.1 .0 46.0	100.0 99.7	26.9 26.9 .0		744	690	201	35.7
	303 SYSTEM 302	100.0 100.0 100.0 99.9	29.1 29.1 .0	100.0 99.7	26.9 26.9 .0					
2/84	303 SYSTEM 302 303 SYSTEM 302	100.0 100.0 100.0 99.9 100.0	29.1 29.1 .0 46.0 46.0	99.7 99.7	26.9 26.9 .0 46.0 46.0					
2/84	303 SYSTEM 302 303 SYSTEM 302 303	100.0 100.0 100.0 99.9 100.0 100.0	29.1 29.1 .0 46.0 46.0	99.7 99.7 100.0 100.0	26.9 26.9 .0 46.0 46.0					
2/84	303 SYSTEM 302 303 SYSTEM 302	100.0 100.0 100.0 99.9 100.0 100.0	29.1 29.1 .0 46.0 46.0	99.7 99.7 100.0 100.0	26.9 26.9 .0 46.0 46.0				320	
2/84 3/84	303 SYSTEM 302 303 SYSTEM 302 303	100.0 100.0 100.0 99.9 100.0 100.0	29.1 29.1 .0 46.0 46.0	99.7 99.7 99.7 100.0 100.0	26.9 26.9 .0 46.0 46.0 .5 45.5		696	696	320	50.0
2/84 3/84	303 SYSTEM 302 303 SYSTEM 302 303 SYSTEM	100.0 100.0 100.0 99.9 100.0 100.0	29.1 29.1 .0 46.0 46.0 .5 51.4 51.9	99.7 99.7 99.7 100.0 100.0	26.9 26.9 .0 46.0 46.0 45.5 45.5		696	696	320	50.0
2/84 3/84	303 SYSTEM 302 303 SYSTEM 302 303 SYSTEM 302	100.0 100.0 99.9 100.0 100.0 100.0	29.1 29.1 .0 46.0 46.0 .5 51.4 51.9	99.7 99.7 100.0 100.0	26.9 26.9 .0 46.0 46.0 .5 45.5		696	696	320 342	50.0
2/84 3/84	303 SYSTEM 302 303 SYSTEM 302 303 SYSTEM 302 303	100.0 100.0 99.9 100.0 100.0 100.0 100.0	29.1 29.1 .0 46.0 46.0 .5 51.4 51.9	99.7 99.7 100.0 100.0 100.0	26.9 26.9 .0 46.0 46.0 .5 45.5 45.9 .0 18.1 18.1		696 744	696 659	320 342	50.0 45.6
2/84 3/84 4/84	303 SYSTEM 302 303 SYSTEM 302 303 SYSTEM 302 303 SYSTEM	100.0 100.0 99.9 100.0 100.0 100.0 100.0	29.1 29.1 .0 46.0 46.0 .5 51.4 51.9 .0 91.6 91.6	100.0 99.7 99.7 100.0 100.0 100.0 100.0	26.9 26.9 .0 46.0 46.0 .5 45.5 45.9 .0 18.1 18.1		696 744	696 659	320 342	50.0 45.6
2/84 3/84 4/84	303 SYSTEM 302 303 SYSTEM 302 303 SYSTEM 302 303 SYSTEM 302	100.0 100.0 99.9 100.0 100.0 100.0 100.0 100.0	29.1 29.1 .0 46.0 46.0 .5 51.4 51.9 .0 91.6 91.6	99.7 99.7 100.0 100.0 100.0	26.9 26.9 .0 46.0 46.0 .5 45.5 45.9 .0 18.1 18.1		696 744	696 659	320 342 131	50.0 45.6
2/84 3/84 4/84	303 SYSTEM 302 303 SYSTEM 302 303 SYSTEM 302 303 SYSTEM 302 303 SYSTEM	100.0 100.0 99.9 100.0 100.0 100.0 100.0 100.0 100.0 100.0	29.1 29.1 .0 46.0 46.0 .5 51.4 51.9 .0 91.6 91.6	100.0 99.7 99.7 100.0 100.0 100.0 100.0 100.0 100.0	26.9 26.9 .0 46.0 46.0 .5 45.5 45.9 .0 18.1 18.1		696 744 720	696 659 143	320 342 131	50.0 45.6 10.7
2/84 3/84 4/84	303 SYSTEM 302 303 SYSTEM 302 303 SYSTEM 302 303 SYSTEM 302 303 SYSTEM	100.0 100.0 99.9 100.0 100.0 100.0 100.0 100.0 100.0 100.0	29.1 29.1 .0 46.0 46.0 .5 51.4 51.9 .0 91.6 91.6 69.3 27.7 97.0 IONS/COMMENTS	100.0 99.7 99.7 100.0 100.0 100.0 100.0 100.0 100.0	26.9 26.9 .0 46.0 46.0 .5 45.5 45.9 .0 18.1 18.1	-RELATED PRO	696 744 720 744	696 659 143 473	320 342 131 459	50.0 45.6 10.7
2/84 3/84 4/84	303 SYSTEM 302 303 SYSTEM 302 303 SYSTEM 302 303 SYSTEM 302 303 SYSTEM	100.0 100.0 99.9 100.0 100.0 100.0 100.0 100.0 100.0 100.0 77.4 100.0	29.1 29.1 .0 46.0 46.0 .5 51.4 51.9 .0 91.6 91.6 69.3 27.7 97.0 IONS/COMMENTS	100.0 99.7 99.7 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0	26.9 26.9 .0 46.0 46.0 .5 45.5 45.9 .0 18.1 18.1 44.1 17.6 61.7	-RELATED PRO	696 744 720 744	696 659 143 473	320 342 131 459	50.0 45.6 10.7
2/84 3/84 4/84 5/84	303 SYSTEM 302 303 SYSTEM 302 303 SYSTEM 302 303 SYSTEM 302 303 SYSTEM ** PROBLE	100.0 100.0 99.9 100.0 100.0 100.0 100.0 100.0 100.0 100.0	29.1 29.1 .0 46.0 46.0 .5 51.4 51.9 .0 91.6 91.6 69.3 27.7 97.0 IONS/COMMENTS	100.0 99.7 99.7 100.0 100.0 100.0 100.0 100.0 100.0	26.9 26.9 .0 46.0 46.0 .5 45.5 45.9 .0 18.1 18.1 44.1 17.6 61.7	-RELATED PRO	696 744 720 744	696 659 143 473	320 342 131 459	50.0 45.6 10.7

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

ON JUNE 24, MODULE 302 WAS TAKEN OUT OF SERVICE FOR PACKING REPAIRS AND REMAINED OUT OF SERVICE FOR THE REST OF THE MONTH.

744 744 327 82.0

** PROBLEMS/SOLUTIONS/COMMENTS

MAINTENANCE WAS COMPLETED ON MODULE 303 AND IT WAS PLACED BACK INTO SERVICE ON JULY 4, 1984.

MODULE 302 WAS UNAVAILABLE FOR SERVICE DURING THE MONTH DUE TO ABSORBER PACKING REPAIRS.

8/84 SYSTEM 744 9/84 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR AUGUST AND SEPTEMBER 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

ARIZONA PUBLIC SERVICE COMPANY NAME PLANT NAME CHOLLA UNIT NUMBER JOSEPH CITY CITY ARIZONA STATE 84. (.196 LB/MMBTU) 430. (1.000 LB/MMBTU) 344. (.800 LB/MMBTU) REGULATORY CLASSIFICATION PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW 119 115 119 119 NET UNIT GENERATING CAPACITY W/FGD - MW NET UNIT GENERATING CAPACITY WO/FGD - MW EQUIVALENT SCRUBBED CAPACITY MW ** UNIT DATA - BOILER AND STACK COMBUSTION ENGINEERING BOILER SUPPLIER BOILER TYPE PULVERIZED COAL BOILER SERVICE LOAD BASE 226.51 (480000 ACFM)
135.6 (276 F)
76. (250 FT)
CONCRETE
3.7 (12.0 FT) DESIGN BOILER FLUE GAS FLOW - CU.M/S
BOILER FLUE GAS TEMPERATURE - C STACK HEIGHT - M STACK SHELL STACK TOP DIAMETER - M ** FUEL DATA FUEL TYPE COAL FUEL GRADE BITUMINOUS AVERAGE HEAT CONTENT J/G 23609. (10150 BTU/LB) RANGE HEAT CONTENT - BTU/LB AVERAGE ASH CONTENT - % 9650-10600 13.50 9.7-22.5 RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - % 15.00 RANGE MOISTURE CONTENT % ***** AVERAGE SULFUR CONTENT - % .50 RANGE SULFUR CONTENT - % 0.4-1.0 AVERAGE CHLORIDE CONTENT - % .02 RANGE CHLCRIDE CONTENT - % 0.01-0.04 *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER 1 NUMBER OF SPARES D TYPE CYCLONE RESEARCH-COTTRELL SUPPLIER INLET FLUE GAS CAPACITY - CU.M/S 226.5 (480000 ACFM) 135.6 (276 F) INLET FLUE GAS TEMPERATURE - C PARTICLE REMOVAL EFFICENCY -% 75.0 ** ESP NUMBER 0 TYPE NONE ** PARTICLE SCRUBBER NUMBER 2 INITIAL START-UP DATE 10/73 GENERIC TYPE VENTURI TOWER SFECIFIC TYPE VARIABLE-THROAT/BOTTOM-ENTRY LIQUID DISTRIBUTION TRADE NAME/COMMON NAME FLOODED DISC SCRUBBER SUPPLIER RESEARCH-COTTRELL DIMENSIONS - FT 6.0 DIA X 45.0 SHELL GENERIC MATERIAL STAINLESS STEEL SHELL SPECIFIC MATERIAL AUSTENITIC ORGANIC LINER GENERIC MATERIAL LINER SPECIFIC MATERIAL MAT-REINFORCED EPOXY NUMBER OF CONTACTING ZONES NONE NUMBER OF CONTACTING ZONES 1 LIQUID RECIRCULATION RATE - LITER/S 336.4 (5340 GPM)

ARIZONA PUBLIC SERVICE: CHOLLA 1 (CONT.)

```
(22.0 GAL/1000ACF)
L/G RATIO - LITER/CU.M
                                           2.9
PH CONTROL ADDITIVE
                                        ABSORBER SLURRY [TRAIN A ONLY]
PRESSURE DROP - KPA
                                                 (15.0 IN-H2O)
                                          3.7
INLET GAS FLOW RATE - CU.M/S
                                          113.3
                                                      ( 240000 ACFM)
                                                      ( 278 F)
INLET GAS TEMPERATURE - C
                                         136.7
PARTICLE REMOVAL EFFICIENCY - %
                                           99.2
```

*** FGD SYSTEM

** GENERAL DATA

SALEABLE PRODUCT/THROWAWAY PRODUCT THROWAWAY PRODUCT SO2 REMOVAL MODE WET SCRUBBING PROCESS TYPE LIMESTONE PROCESS ADDITIVES NONE SYSTEM SUPPLIER RESEARCH-COTTRELL A-E FIRM **EBASCO** DEVELOPMENT LEVEL FULL SCALE NEW/RETROFIT RETROFIT UNIT DESIGN SO2 REMOVAL EFFICIENCY - % 55.00 ENERGY CONSUMPTION - % 3.4 CURRENT STATUS 12/73 COMMERCIAL START-UP INITIAL START-UP 10/73 CONTRACT AWARDED 7/71

** DESIGN AND OPERATING PARAMETERS

PARTICLE REMOVAL EFFICENCY - %

NUMBER OF CONTACTING ZONES

OPER. & MAINT. REQUIREMENT - MANHR/DAY 40.0

** QUENCHER/PRESATURATOR

NUMBER

** ABSORBER

NUMBER GENERIC TYPE COMBINATION TOWER SPECIFIC TYPE SPRAY/PACKED TRADE NAME/COMMON TYPE N/A RESEARCH-COTTRELL SUPPLIER 22.0 DIA X 70.0 DIMENSIONS - FT SHELL GENERIC MATERIAL STAINLESS STEEL AUSTENTITC SHELL SPECIFIC MATERIAL TYPE 316L SHELL MATERIAL TRADE NAME/COMMON TYPE NONE LINER GENERIC MATERIAL LINER SPECIFIC MATERIAL LINER MATERIAL TRADE NAME/COMMON TYPE N/A GAS CONTACTING DEVICE TYPE VERTICAL CROSS CHANNEL FIXED GRID PACKING NUMBER OF CONTACTING ZONES DISTANCE BETWEEN GAS CONTACTING ZONES - CM 61.0 (24.0IN) (9300 GPM) LIQUID RECIRCULATION RATE - LITER/S 586. 6.0 (45.0 GAL/1000 ACF) L/G RATIO - L/CU.M (.5 IN-H20) (6.9 FT/S) GAS-SIDE PRESSURE DROP - KPA .1 SUPERFICAL GAS VELOCITY - M/SEC 2.1 (205000 ACFM) 96.74 INLET GAS FLOW - CU. M/S 50.0 (122 F) INLET GAS TEMPERATURE C SO2 REMOVAL EFFICIENCY - X

92.0

99.7

0

** ABSORBER

NUMBER SPRAY TOWER GENERIC TYPE OPEN COUNTERCURRENT SPRAY SPECIFIC TYPE TRADE NAME/COMMON TYPE N/A RESEARCH-COTTRELL SUPPLIER DIMENSIONS - FT 22.0 DIA X 70.0 SHELL GENERIC MATERIAL STAINLESS STEEL **AUSTENITIC** SHELL SPECIFIC MATERIAL SHELL MATERIAL TRADE NAME/COMMON TYPE TYPE 316L NONE LINER GENERIC MATERIAL LINER SPECIFIC MATERIAL N/A LINER MATERIAL TRADE NAME/COMMON TYPE N/A GAS CONTACTING DEVICE TYPE NONE

1

ARIZONA PUBLIC SERVICE: CHOLLA 1 (CONT.)

```
586. ( 9300 GPM)
6.0 ( 45.0 GAL/1000 ACF)
.1 ( .5 IN-H20)
2.1 ( 6.9 FT/S)
   LIQUID RECIRCULATION RATE - LITER/S
                                                586.
   L/G RATIO - L/CU.M
   GAS-SIDE PRESSURE DROP - KPA
   SUPERFICAL GAS VELOCITY - M/SEC
                                                            ( 205000 ACFM)
( 122 F)
   INLET GAS FLOW - CU. M/S
                                                 96.74
                                                 50.0
   INLET GAS TEMPERATURE - C
   SO2 REMOVAL EFFICIENCY - %
                                                25.0
** MIST FLIMINATOR
                                              PRIMARY COLLECTOR
   PRE-MIST ELIMINATOR/MIST ELIMINATOR
   NUMBER PER SYSTEM
                                              2
   NUMBER PER MODULE
                                               1
   GENERIC TYPE
                                              CYCLONIC
                                              CYCLONIC SEPARATOR
   SPECIFIC TYPE
                                              CYCLONIC TOWER
   TRADE NAME/COMMON TYPE
   CONFIGURATION
                                              VERTICAL
   NUMBER OF STAGES
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              STAINLESS STEEL
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                             AUSTENITIC
   WASH WATER SOURCE
                                              NONE
   WASH FREQUENCY
                                              N/A
** REHEATER
   NUMBER
                                               2
   NUMBER PER MODULE
                                               1
                                              IN-LINE
   GENERIC TYPE
   SPECIFIC TYPE
                                              STEAM
   TRADE NAME/COMMON TYPE
                                              BARE TUBE
                                              SEPARATE VESSEL AFTER ABSORBER
    LOCATION
    TEMPERATURE INCREASE C
                                                22.2 ( 40 F)
115.62 ( 245000 ACFM)
    INLET FLUE GAS FLOW RATE - CU. M/S
                                               115.62
    INLET FLUE GAS TEMPERATURE - C
                                               48.9
                                                            ( 120 F)
( 160 F)
    OUTLET FLUE GAS TEMPERATURE - C
                                                 71.1
    NUMBER OF BUNDLES PER BANK
                                                 3
                                           STAINLESS STEEL
    CONSTRUCTION MATERIAL GENERIC TYPE
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                            AUSTENITIC
** FANS
   NUMBER
                                               2
   NUMBER OF SPARES
                                               n
    DESIGN
                                              CENTRIFUGAL
    SUPPLIER
                                              WESTINGHOUSE
    FUNCTION
                                              UNIT
    APPLICATION
                                              FORCED DRAFT
    SERVICE
                                              DRY
    FLUE GAS FLOW RATE - CU.M/S
                                              113.26 ( 240000 ACFM)
    FLUE GAS TEMPERATURE C
                                               135.6
                                                            ( 276 F)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                           CARBON STEEL
** FANS
   NUMBER
                                               2
    NUMBER OF SPARES
                                               0
    DESIGN
                                              CENTRIFUGAL
    SUPPLIER
                                              WESTINGHOUSE
    FUNCTION
                                              BOOSTER
    APPLICATION
                                              FORCED DRAFT
    SERVICE
                                              DRY
    FLUE GAS FLOW RATE - CU.M/S
                                              113.26 ( 240000 ACFM)
    FLUE GAS TEMPERATURE C
                                               135.6
                                                             ( 276 F)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                              CARBON STEEL
** DAMPERS
    NUMBER
   FUNCTION
                                              SHUT-OFF
    GENERIC TYPE
                                              GUILLOTINE
    SPECIFIC TYPE
                                              NΩ
    CONSTRUCTION MATERIAL GENERIC TYPE
                                              STAINLESS STEEL
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              AUSTENITIC
   LINER GENERIC MATERIAL TYPE
                                              NONE
   LINER SPECIFIC MATERIAL TYPE
                                              N/A
```

ARIZONA PUBLIC SERVICE: CHOLLA 1 (CONT.)

** DAMPERS

NUMBER
FUNCTION
GENERIC TYPE
SPECIFIC TYPE

CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE

** DAMPERS

NUMBER
FUNCTION
GENERIC TYPE
SPECIFIC TYPE
CONSTRUCTION MATER

CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE

** DAMPERS

NUMBER
FUNCTION
GENERIC TYPE
SPECIFIC TYPE

CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

** DAMPERS

NUMBER FUNCTION GENERIC TYPE SPECIFIC TYPE

CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE

** DUCTWORK

LOCATION
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

** DUCTWORK

LOCATION

SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE

** DUCTWORK

LOCATION
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

** REAGENT PREPARATION EQUIPMENT

FUNCTION DEVICE DEVICE TYPE NUMBER 2 SHUT-OFF GUILLOTINE

NR

STAINLESS STEEL AUSTENITIC NONE N/A

2

SHUT-OFF GUILLOTINE NR

STAINLESS STEEL AUSTENITIC NONE

N/A

2 CONTROL LOUVER NR

STAINLESS STEEL AUSTENITIC NONE

N/A

2 CONTROL LOUVER NR

STAINLESS STEEL AUSTENITIC NONE N/A

SCRUBBER INLET CARBON STEEL AISI 1110 NONE

N/A

SCRUBBER OUTLET TO REHEATER CARBON STEEL

CARBON STEEL
AISI 1110
ORGANIC

MICA FLAKE-FILLED POLYESTER

BYPASS

CARBON STEEL AISI 1110 NONE N/A

NONE N/A N/A 0

ARIZONA PUBLIC SERVICE: CHOLLA 1 (CONT.)

** TANKS NUMBER SERVICE 1 SCRUBBER RECYCLE WASTE SLURRY BLEED 7 ABSORBER RECYCLE REAGENT PREP PRODUCT ** PUMPS NUMBER SERVICE ٦ SCRUBBER RECIRCULATION ABSORBER RECIRCULATION MIST ELIMINATOR WASH ** SOLIDS CONCENTRATING/DEWATERING NONE DEVICE *** SLUDGE 87.0 MOISTURE CONTENT - % TOTAL FREE WATER ** TREATMENT BLEED METHOD N/A DEVICE PROPRIETARY PROCESS N/A ** DISPOSAL FINAL NATURE POND TYPE ON-SITE LOCATION SITE TRANSPORTATION METHOD PIPELINE NONE SITE TREATMENT 70-100 ACRES X 6 FT DEEP SITE DIMENSIONS 623730 (510.0 ACRE-FT) SITE CAPACITY - CU.M ** PROCESS CONTROL AND INSTRUMENTATION SCRUBBER AND ABSORBER HOLD TANK PROCESS STREAM CHEMICAL PARAMETERS PH 5.2 IN SCRUBBER HOLD TANK, 6.5 IN ABSORBER HO CONTROL LEVELS MANUAL PROCESS CONTROL MANNER ** WATER BALANCE OPEN HATER LOOP TYPE 7.6 (120 GPM) MAKEUP WATER ADDITION - LITERS/S ** CHEMICALS AND CONSUMPTION ABSORBENT FUNCTION NAME LIMESTONE SOURCE/SUPPLIER SUPERIOR CO. POINT OF ADDITION ABSORBER RECYCLE TANK ** FGD SPARE CAPACITY INDICES ABSORBER - % . 0 ** FGD SPARE COMPONENT INDICES ABSORBER .0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS HOURS FACTOR

744 10/73 SYSTEM

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

INITIAL TESTING OF THE FGD SYSTEM BEGAN ON OCTOBER 2, 1973. THE SYSTEM OPERATED UNTIL THE SCHEDULED SHUTDOWN DATE OF OCTOBER 21. DURING THE THREE WEEK TEST PERIOD, PARTICULATE MATTER AND SO2 REMOVAL EFFICIENCIES, MIST CARRYOVER FROM THE TOWERS, MAXIMUM PROCESS GAS FLOW RATES, AND BYPASS GAS LEAKAGE RATES WERE DETERMINED.

THE DATA COLLECTED INCLUDED THE FOLLOWING:

FLOODED DISC SCRUBBER SO2 REMOVAL EFFICIENCY (MODULE A): 92% SPRAY TOWER SCRUBBER SO2 REMOVAL EFFICIENCY (MODULE B): 25%

UNIT OVERALL SO2 REMOVAL EFFICIENCY: 58.5%

MIST CARRYOVER FROM MODULES A AND B: 0%

SOLIDS CARRYOVER FROM MODULE A: 0.005 GR/SCF

AIR LEAKAGE INTO SYSTEM DOWNSTREAM OF SCRUBBERS: 18,400 ACFM CHLORIDE ION CONCENTRATION IN FLOODED DISC SCRUBBER RECIRCULATION: 1600 PPM

CHLORIDE ION CONCENTRATION IN SPRAY TOWER RECIRCULATION: 575 PPM CHLORIDE ION CONCENTRATION IN SCRUBBER MAKEUP WATER (COOLING TOWER BLOWDOWN): 933 PPM

CHLORIDE LEVELS ARE SUFFICIENT TO CAUSE PITTING CORROSION IN LOCALIZED AREAS WHEN TEMPERATURES ARE GREATER THAN 140F AND PH IS LESS THAN 3.0.

11/73 SYSTEM 720

12/73 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE CONSTRUCTION AND INITIAL TESTING OF THE SYSTEM WERE COMPLETED ON DECEMBER 3. COMMERCIAL OPERATIONS BEGAN ON DECEMBER 14.

BECAUSE OF A DIFFERENCE IN THE SIZE OF THE MAIN DUCT AND REHEATED TRANSITION DUCT, THE GAS FLOW PRODUCES HARMONIC VIBRATIONS IN THE REHEATER. THE VIBRATIONS WERE PARTIALLY DAMPENED BY INSTALLATION OF BAFFLES.

ONE OF THE REHEATER BUNDLES WAS BADLY CORRODED BY ACID THAT CONDENSED IN THE UNINSULATED DUCT UPSTREAM OF THE REHEATERS. THE TUBE BUNDLE WAS REPLACED AND A BAFFLE WAS INSTALLED TO DIVERT CONDENSED ACID FROM REHEATER TUBES.

THE DUCT UPSTREAM OF THE REHEATER WAS INSULATED. THE ACID CONDENSATION OCCURRED ONLY IN THE B-MODULE WHICH CONTAINS NO INTERNAL FACKING AND CONSEQUENTLY HAS A LOWER DEGREE OF SULFUR DIOXIDE REMOVAL (25%).

SOME LINES PLUGGED, PARTICULARLY WHEN THE SYSTEM OPERATED AT LOW FLOW RATES.

SOLIDS SETTLED OUT IN STANDBY PUMPS, AND EXCESSIVE FAN VIBRATIONS OCCURRED BECAUSE OF ACCUMULATION OF SCALE BUILDUP WHEN THE UNIT WAS IDLE. TO SOLVE THESE PROBLEMS THE PACKING GLAND POSITION WAS REVERSED (INSTALLED UPSIDE DOWN). THE FAN WAS SANDBLASTED. THE PIPING WAS MODIFIED TO ELIMINATE STAGNANT POCKETS, AND PUMPS WERE FLUSHED IMMEDIATELY AFTER REMOVAL FROM SERVICE.

THE UTILITY EXPERIENCED SOLIDS BUILDUP IN THE FDS STUFFING GLAND BOX AND ON TOP OF THE SPRAY DOME.

1/74 A 97.0 B 90.0

SYSTEM 93.5 744

2/74 A 100.0

				PERFORMA	VCE DATA					
PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% REI	MOVAL PART.		BOILER HOURS	CAP. FACTOR
	B SYSTEM			94.0 97.0				672		
3/74	A B SYSTEM			100.0 66.0 83.0				744		
4/74	A B SYSTEM			66.0 57.0 61.5				720		

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM PERFORMED SATISFACTORILY FROM DECEMBER 15, 1973 TO APRIL 15, 1974. ALTHOUGH SEVERAL UPSETS CAUSED SHUTDOWN OF ONE OR BOTH MODULES FOR SHORT PERIODS SYSTEM AVAILABILITY AVERAGED 92.6% DURING THAT PERIOD.

THE SCRUBBER MODULES WERE SHUTDOWN FOR SHORT PERIODS IN APRIL TO REPLACE CORRODED COR-TEN STEEL EXPANSION JOINTS ON THE REHEATER BUNDLES. MODULE A WAS DOWN APRIL 17 THROUGH 27. MODULE B WAS DOWN APRIL 15 THROUGH 28.

5/74	A B SYSTEM			98.0 99.0 98.5		744	744	
6/74	A B SYSTEM			100.0 100.0 100.0		72 0		
7/74	A B SYSTEM		97.5 98.5 98.0	97.0 92.0 94.5	97.5 98.5 98.0	744	744	729
8/74	A B SYSTEM	100.0	94.5 100.0 97.3	97.0 100.0 98.5	94.5 100.0 97.3	744	744	724

** PROBLEMS/SOLUTIONS/COMMENTS

EACH MODULE WAS OUT OF SERVICE ONE DAY OVER THE MONTH FOR THE INSTALLATION OF BAFFLE PLATES IN THE INLET DUCT OF EACH REHEATER. THE BAFFLE INSTALLATIONS WERE PARTLY SUCCESSFUL IN STOPPING REHEATER VIBRATION PROBLEMS.

9/74	A	95.0	
	В	99.0	
	SYSTEM	97.0	720
10/74	A	83.0	
	В	68.0	
	SYSTEM	75.5	744

** PROBLEMS/SOLUTIONS/COMMENTS

THE SYSTEM WAS SHUT DOWN IN LATE OCTOBER FOR AN ANNUAL BOILER AND FGD SYSTEM OVERHAUL.

DURING THE OUTAGE SEVERAL INSTANCES OF PITTING CORROSION WERE DISCOVERED IN THE 316L SS FLOODED DICS SCRUBBER WALLS.

REHEATER TUBE LEAKS WERE DISCOVERED IN THE B-SIDE REHEATER DURING THE OUTAGE.

11/74 A 100.0

				PERFORMAI	NCE DATA						
		AVAILABILITY				% REM	OVAL	PER	BOILER		CAP. FACTOR
	B SYSTEM			98.0 99.0				720			
12/74	A B SYSTEM			100.0 100.0 100.0				744			
1/75	A B SYSTEM		97.7 98.7 98.2	97.7 98.7 98.2	97.7 98.7 98.2			744	744	730	

** PROBLEMS/SOLUTIONS/COMMENTS

OPERATION OF THE SYSTEM THROUGHOUT 1975 AND 1976 WAS ACCOMPANIED BY A NUM-BER OF MINCR PROBLEM AREAS INCLUDING: SIGNIFICANT CORROSION ATTACK IN THE VESSEL WALLS OF THE VENTURI FLOODED-DISC PARTICULATE SCRUBBER MODULE; ACID CORROSION IN THE B-SIDE REHEATER HOUSING; SCALE BUILDUP IN THE PIPE OUTLET AT THE SLUDGE/FLYASH EVAPORATION POND; PLUGGING IN THE SCRUBBER TOWER PACK ING AND MIST ELIMINATOR; EROSION IN THE PUMPS; CORROSION IN THE BOILER EX-HAUST ELBOW OF THE DUCTWORK LEADING FROM THE SCRUBBERS TO THE STACK.

DURING JANUARY THE BYPASS SYSTEM EXPERIENCED CONTROL PROBLEMS. NO SOLUTION HAS YET BEEN FOUND.

A LEAK IN THE B-SIDE ABSORBER TOWER WAS WELDED IN JANUARY.

SOME LEAKS WERE DISCOVERED OVER THE MOUTH ON THE A-SIDE VENTURI THROATS. THE LEAKS WERE ATTRIBUTED TO NORMAL WEAR.

LEAKS WERE DISCOVERED IN THE B-SIDE REHEATER DUCTS IN JAUNARY.

2/75	A	95.5	95.5	95.5			
	В	91.4	91.4	91.4			
	SYSTEM	93.5	93.5	93.5	672	672	628

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT PROBLEMS WITH VESSEL LEAKS CONTINUED THROUGH FERRUARY.

SOME OUTAGE TIME WAS REQUIRED FOR RECYCLE PUMP REPAIRS OVER THE MONTH.

THE UTILITY DISCOVERED SOME ADDITIONAL EROSION/CORROSION PROBLEMS IN THE FGD SYSTEM IN FEBRUARY.

3/75 SYSTEM 744

** PRCBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT BUILDUP OF SEDIMENT HAS OCCURRED SEVERAL TIMES SINCE STARTUP IN DEAD SPACES, IN PIPE LINES, AND VALVES OF IDLE PUMPS AS WELL AS IN PROCESS LINES DURING PERIODS OF REDUCED OPERATING RATE.

SOME PIPE LINERS HAVE EXPERIENCED EROSION SINCE STARTUP. THE EROSION WAS DUE IN SOME CASES TO UNSATISFACTORY LINER MATERIALS AND IN OTHER CASES TO HIGH VELOCITIES THROUGH PIPES AND FITTINGS. PIPING MODIFICATIONS HELPED TO REDUCE THE EROSION PROBLEM. CRACKING OF THE RUBBER LINING IN SOME PIPES WAS DUE TO DEFECTS IN FABRICATION.

SOME FLOODED DISC SCRUBBER PACKING PLUGGING HAS OCCURRED. IT APPEARS THAT THIS IS A RESULT OF THE GRADE OF COAL BURNED. THE "WETTED FILM CONTACTOR" PACKING LIFE HAS BEEN REDUCED.

4/75 A 88.5 88.5 82.4

PERIOD	MODULE AV	AILABILITY	OPERABILITY	RELIABILITY	UTILIZATION				BOILER HOURS		
	в		65.2		60.7						
	SYSTEM		76.9		71.6			720	67 0	515	
	** PROBLE	MS/SOLUTIO	NS/COMMENTS								
			HE UTILITY RE	PORTED THAT	THERE ARE ST	ILL PR	ROBLEM	S WITH	THE BY	PASS SY	STEM
					ED TO REPAIR TOWER PACKING			PIPING	OT DNA	UNPLUG	;
		Т	HE REHEATER S	SECTION WAS	AGAIN PATCHED	HTIW	CEILC	OTE DUR	ING APP	RIL.	
5/75			47.5	47.5	47.5						
	B SY STEM		39.9 43.7	39.9 43.7	39.9 43.7			744	744	325	
		MS/SOLUTIO	NS/COMMENTS		1317			,,,,	7-1-1	323	
				WERE OUT OF	SERVICE FOR	MOST O	F THE	MONTH	בא דו	. SCHEU	III ED
					LD BE UNDERTA			71011111	50 ma	30,120	0225
6/75		100.0	100.0	100.0	100.0						
	B SYSTEM	100.0 100.0	100.0 100.0	100.0 100.0	100.0 100.0			720	720	720	
			NS/COMMENTS	20000	200.0			720	720	720	
				AMOUNT OF I	PLUGGING WAS	ORSEDV	EN TH	THE MO	DILLE A	ABCODD	ED.
			TOWER PACKING		- LOGOTING WAS	DOSERV	20 14	ותב וזכ	NOCE A	ADSUKB	CK
			PLUGGING OCCL	RRED IN MIS	T ELIMINATORS						
			NO MAJOR PROE	LEMS WERE EN	COUNTERED DU	RING T	HE PE	RIOD.			
7/75			97.5	97.5	97.5						
	B SYSTEM		98 .5 98 .0	98.5 98.0	98.5 98.0				-		
		1S/S01.UTT0	NS/COMMENTS	70.0	70.0			744	744	729	
	, ,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,			SHUT DOWN TO	CLEAN FLOW	RESTRI	CTION	S IN FL	.00DED-0	ISC RE	CIR-
8/75											
0//3	A B	100.0	94.5 100.0	94.5 100.0	94.5 100.0						
	SYSTEM		97.3	97.3	97.3			744	744	724	
	** PROBLE	1S/SOLUTIO	NS/COMMENTS								
			THE A-SIDE WA	S SHUT DOWN	FOR INSPECTION	ON.					
9/75	A		64.5	97.6	64.5						
	B SYSTEM		93.0	97.4	93.0						
		15/50111770	78.8 NS/COMMENTS	97.5	78.8			720	720	567	
				RECUITED FO	N DI 110000						
			LINES.	KESULIED FRO	DM PLUGGED FLO	JODEĐ	nizc ;	SCRUBBE	R RECIR	CULATI	ОИ
10/75	A		78.0	84.0	56.4						
	_		,	01.0	30.4						
	B SYSTEM		24.6 51.3	54.8 69.4	17.8 37.1			744	538	276	

744

SYSTEM

PERIOD	MODULE AVAILABILI	TY OPERABILITY	RELIABILITY	UTILIZATION				BOILER HOURS		CAP. FACTOR
	** PROBLEMS/SOLUT	TONS /COMMENTS								
	** FRODELIIS/ SOLOT	101437 CONTILITY'S								
		OUTAGES RESU SELS.	LTED FROM SC	HEDULED EQUIF	MENT	OVERHA	ULS AN	D RECOA	TING O	F VES-
11/75		100.0	100.0	100.0						
	B System	71.4 85.7	80.0 90.0	71.4 85.7			720	720	617	
	** PROBLEMS/SOLUT	IONS/COMMENTS								
		NO MAJOR OUT	AGES OR PROB	LEMS OCCURRED	DURI	NG THE	REPOR	T PERIU	o.	
12/75	A	100.0	100.0	100.0						
	B SYSTEM	100.0 100.0	100.0 100.0	100.0 100.0			744	744	744	
	** PROBLEMS/SOLUT	IONS/COMMENTS		•						
		MINOR PROBLE	MS ENCOUNTER	ED REQUIRED R	RECYCL	E PUMP	REBUI	LDING.		
		THE B-SIDE R	EHEATER COIL	. MALFUNCTIONE	D BUT	NO 0U	TAGE T	IME WAS	REQUI	RED.
1/76	A	96.0	98.9	96.0						
	B System	87.9 92.0	98.6 98.8	89.9 92.0			744	744	684	
	** PROBLEMS/SOLUT	IONS/COMMENTS								
		MINOR VALVE	PLUGGING OCC	URRED.						
		MINOR RECIRC	ULATION LINE	PLUGGING OCC	URRED	•				
		MODULE B OPE	RATING HOURS	WERE LOWER E	BECAUS	E OF R	EDUCED	SYSTEM	REQUI	REMENTS
2/76	SYSTEM						696			
3/76	SYSTEM						744			
	** PROBLEMS/SOLUT	IONS/COMMENTS								
		INFORMATION	WAS UNAVAILA	BLE FOR THE 1	10NTHS	OF FE	BRUARY	AND MA	RCH.	
4/76	A		99.0							
	B SYSTEM		97.4 98.2				720			
	** PROBLEMS/SOLUT	TIONS/COMMENTS								
				TLY EXPERIENCE TO			G FAIL	URES IN	THE E	LBOW OF
		THE UTILITY REHEATER.	PERFORMED SO	ME MINOR REPA	AIRS T	O THE	HOUSIN	G OF TH	E B-SI	DE
5/76			76.4							
	B System		99.6				766			

88.0

UTILITY FGD SURVEY: OCTOBER 1983 - SEPTEMBER 1984

ARIZONA PUBLIC SERVICE: CHOLLA 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

CORROSION AND PLUGGING PROBLEMS OCCURRED ON THE A-SIDE REHEATER TUBES.

THE UTILITY REPORTED THAT PLUGGING OCCURRED IN THE FLOODED DISC SCRUBBER RECIRCULATION LINES.

PLUGGING OCCURRED IN THE FLOODED DISC SCRUBBER PACKING.

PLUGGING OCCURRED IN THE MIST ELIMINATORS.

HEAVY PUMP MAINTENANCE WAS REQUIRED IN MAY. THE UTILITY NOW CONSIDERS HEAVY PUMP MAINTENANCE NORMAL FOR THE CHOLLA 1 SCRUBBER.

6/76 A 64.1 B 39.4 SYSTEM 51.8

** PROBLEMS/SOLUTIONS/COMMENTS

LOW RELIABILITY FACTORS FOR THE MONTH OF JUNE RESULTED FROM A SCHEDULED MID-YEAR SCRUBBER SHUTDOWN FOR MAINTENANCE, INSPECTION AND REPAIRS.

SOME SCALING AND CORROSION PROBLEMS WERE UNCOVERED IN THE SCRUBBING SYSTEM RECYCLE TANKS.

720

7/76	A	100.0	
	В	97.5	
	SYSTEM	98.8	744
8/76	A	100.0	
	В	100.0	
	SYSTEM	100.0	744

** PROBLEMS/SOLUTIONS/COMMENTS

REPAIRS TO THE COATING IN THE ELBOW OF THE SCRUBBER EXHAUST DUCT WERE COMPLETED OVER THE JULY-AUGUST PERIOD.

A MALFUNCTIONING SOLENOID VALVE IN THE B-SIDE MIST ELIMINATOR WASH SYSTEM PREVENTING ADEQUATE WASHING, RESULTED IN A MINOR SCRUBBER OUTAGE DURING THE JULY-AUGUST PERIOD.

9/76	A	100.0	100.0	100.0	100.0			
	В		93.9	100.0	93.9			
	SYSTEM		97.0	100.0	97.0	720	720	698

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER WAS IN SERVICE THE ENTIRE MONTH. NO SIGNIFICANT SCRUBBER PROBLEMS WERE REPORTED.

10/76		99.5	56.0	55.8			
	В	66.4	56.0	37.2			
	SYSTEM	83.0	56.0	46.5	744	417	346
11/76	A	94.8	95.8	94.8			
	В	77.2	97.6	77.2			
	SYSTEM	86.1	96.7	86.1	720	720	619

620

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

TWO MINOR FORCED SCRUBBER OUTAGES OCCURRED DURING THE PERIOD.

A REHEATER STEAM LEAK CAUSED A MINOR FORCED OUTAGE.

AN INLET GAS DAMPER ADJUSTMENT PROBLEM IN BOTH THE A-SIDE AND B-SIDE SCRUBBING TRAINS CAUSED A MINOR OUTAGE.

12/76 A 99.8 99.7 99.8 B 67.0 100.0 67.0 SYSTEM 99.9 99.0 83.4 744 744

** PROBLEMS/SOLUTIONS/COMMENTS

ONE OUTAGE WAS REPORTED. THE OUTAGE WAS THE RESULT OF AN ADDITIONAL ADJUSTMENT TO THE A-SIDE GAS INLET DAMPER.

1/77 A 71.6 72.3 71.6 B 91.9 93.4 91.9 SYSTEM 81.8 82.9 81.8 744 744 608

** PROBLEMS/SOLUTIONS/COMMENTS

THE PERFORMANCE INDEX VALUES CONTAINED IN THESE TABLES ARE BASED UPON THE MODULE ACTUAL SERVICE TIME FOR THE PERIOD VERSUS THE NUMBER OF HOURS THE MODULES ARE CALLED UPON TO OPERATE FOR THE SAME PERIOD. THE MODULES OPERATE ON A DEMAND-ONLY BASIS. FLUE GAS IS BYPASSED AROUND THE MODULES WHEN THEY ARE NOT REQUIRED FOR SERVICE.

THE MUNTERS PACKING IN THE A-SIDE TOWER WAS REPLACED IN JANUARY.

BAD C3471 ****

MINOR CORROSION OCCURRED IN THE SYSTEM.

MINOR PLUGGING OF SCRUBBER INTERNALS OCCURRED. THE TOWERS WERE CLEANED.

SCME PROBLEMS OCCURRED WITH THE LIQUID PIPING.

AVERAGE SO2 INLET AND OUTLET CONCENTRATIONS DURING JANUARY WERE 350 PPM AND 175 PPM RESPECTIVELY.

2/77 A 96.5 98.8 96.5 B 88.0 99.6 88.0 SYSTEM 92.2 99.2 92.2 672 672 620

** PROBLEMS/SOLUTIONS/COMMENTS

THERE WERE MECHANICAL DIFFICULTIES WITH THE BY-PASS DAMPERS.

AVERAGE SO2 INLET AND OUTLET VALUES DURING FEBRUARY WERE 350 PPM AND 175 PPM RESPECTIVELY.

3/77 A	71.6	72.3	71.6			
В	91.9	93.4	91.9			
SYSTEM	81.8	82.9	81.8	744	744	608

** PROBLEMS/SOLUTIONS/COMMENTS

THE A-SIDE TOWER PACKING WAS REPLACED DURING MARCH.

BOTH MODULES WERE OUT OF SERVICE FOR CLEANING OF AREAS OF PLUGGING IN THE SCRUBBER INTERNALS DURING THE MONTH.

UTILITY FGD SURVEY: OCTOBER 1983 - SEPTEMBER 1984

ARIZONA PUBLIC SERVICE: CHOLLA 1 (CONT.)

PERIOD	MODULE	AVAILABILITY	OPERABILITY	PERFORMAI RELIABILITY	NCE DATA UTILIZATION	% RE	MOVAL	PER	BOILER HOURS	FGD	CAP.
4/77	A B SYSTEM		99.6 98.6 99.1	100.0 100.0 100.0	88.2 87.3 87.8			720	638	632	

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED NO MAJOR PROBLEMS OCCURRED DURING APRIL.

5/77	A	100.0	87.0	86.7			
	В	100.0	87.0	86.7			
	SYSTEM	100.0	87.0	86.7	744	645	645

** PROBLEMS/SOLUTIONS/COMMENTS

OUTAGE TIME FOR THE BOILER AND FGD SYSTEM WAS A RESULT OF THE SCHEDULED MID-YEAR SCRUBBER CLEANOUT.

DURING MAY RESEARCH-COTTRELL PERSONNEL CONDUCTED FORCED OXIDATION TESTS BY BLOWING AIR INTO THE FLOODED DISC SCRUBBER AND CONVERTING ALL CASO3 TO CASO4 YIELDING SUPERIOR SLUDGE DEWATERING HANDLING AND SCALE-FREE OPERATION.

6/77	A	100.0	100.0	100.0	100.0			
	В	100.0	100.0	100.0	100.0			
	SYSTEM	100.0	100.0	100.0	100.0	720	720	720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED NO MAJOR PROBLEMS FOR THE MONTH OF JUNE.

7/77	A	97.0		
	В	99.0		
	SYSTEM	98.0	744	744

** PROBLEMS/SOLUTIONS/COMMENTS

A MINOR LEAK OCCURRED IN THE LIMESTONE SLURRY TANK.

A MINOR LEAK OCCURRED IN THE B-SIDE RETURN LINE FROM THE FLOODED DISC SCRUBBER TO THE SCRUBBER TANK.

RESEARCH-COTTRELL PERSONNEL ARE STILL ON THE PLANT SITE CONTINUING FORCEDD OXIDATION STUDIES.

8/77	A	97.2	97.2	97.2			
	В	98.6	98.6	98.6			
	SYSTEM	97.9	97.9	97.9	744	744	729

** PROBLEMS/SOLUTIONS/COMMENTS

DOWN TIME WAS REQUIRED TO REPAIR LEAKS IN THE SLURRY DISPOSAL TANK AND THE FLOODED DISC SCRUBBER RETURN LINE BETWEEN THE TOWER AND THE SCRUBBER RECYCLE TANK.

9/77	A	100.0	99.7	100.0	99.7			
	В	100.0	99.7	100.0	99.7			
	SYSTEM	100.0	99.7	100.0	99.7	720	720	718

** PROBLEMS/SOLUTIONS/COMMENTS

ONLY ROUTINE MAINTENANCE WAS REQUIRED FOR THE SCRUBBING SYSTEM DURING SEPTEMBER.

744

0

		AVAILABILITY				% REI	MOVAL	PER	BOILER HOURS	FGD	CAP.
10/77	A	100.0	99.9	100.0	99.9						
	В	100.0	99.9	100.0	99.9						
	SYSTEM	100.0	92.1	98.7	99.9			744	744	743	

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED NO MAJOR PROBLEMS FOR OCTOBER.

11/77	A	100.0	99.7	100.0	23.3			
	В	97.4	84.5	97.4	19.7			
	SYSTEM	98.7	92.0	99.0	21.5	720	169	155

** PROBLEMS/SOLUTIONS/COMMENTS

THE B-SIDE OUTAGE WAS DUE TO LEAKS IN THE VENTURI SECTION OF THE SCRUBBER AND AN EXPANSION JOINT FAILURE IN A RECYCLE PUMP.

THE BOILER OPERATED ONLY 168.5 HOURS BECAUSE OF A SHUTDOWN FOR OVERHAUL IN THE LAST HALF OF NOVEMBER. THE UNIT IS SCHEDULED TO START UP IN MIDDECEMBER.

12/77 SYSTEM .0

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER AND SCRUBBING SYSTEM WERE OUT OF SERVICE THROUGH DECEMBER AS THE OVERHAUL PERIOD CONTINUED.

. 0

OVER THE PAST YEAR EVIDENCE OF CHLORIDE ATTACK WAS NOTED IN THE LIQUID-GAS CENTRIFUGAL SEPARATOR SHELL BELOW THE ABSORBER. THE INTERIOR OF THE VESSEL WAS COATED WITH AN EPOXY MATERIAL BY THE SYSTEM SUPPLIER AS A REMEDY BUT THIS ERODED IN SPOTS AND HAD TO BE REPAIRED. THE EPOXY MATERIAL ALSO ERODED AND DISBONDED BELOW THE SCRUBBER DISC.

DURING 1977 EVIDENCE OF ADDITIONAL CHLORIDE ATTACK WAS NOTED ON THE MODULE B REHEATER TUBES. THE SPRAY DISTRIBUTION DEFLECTOR ABOVE THE FLOODED DISC FAILED BECAUSE OF STRESS-CORROSION CRACKING. THE DEFLECTOR WAS REDESIGNED BY THE SYSTEM SUPPLIER.

EXTENSIVE CORROSION WAS RECENTLY DISCOVERED IN THE DUCTWORK LEADING FROM THE MODULE B ABSORBER TOWER EXHAUST ELBOW TO THE REHEAT TUBE BUNDLE. THE UTILITY HAS RECOATED THE ELBOW SEVERAL TIMES WITH A CEILCOTE LINER. AN APPLICATION PROBLEM CAUSED REPEATED FAILURE OF THE LINER. THIS PROBLEM HAS NOT BEEN FULLY RESOLVED.

1/78	A	97.0	97.0	17.6			
	В	90.9	96.9	16.5			
	SYSTEM	94.0	97.0	17.1	744	135	127

** PROBLEMS/SOLUTIONS/COMMENTS

THE FLOODED DISC SCRUBBER TANK HEADER FOR THE LIMESTONE SLURRY WAS REPAIRED AFTER BEING DAMAGED DURING THE OVERHAUL.

THE BOILER AND SCRUEBER WERE OUT OF SERVICE MOST OF JANUARY AS THE SCHEDULED OVERHAUL CONTINUED.

2/78	A	99.1	100.0	94.7			
	В	87.9	100.0	84.0			
	SYSTEM	93.5	100.0	89.4	672	642	600

		AILABILIT	Y OPERABILITY		UTILIZATION	% REMOVAL	PER I		FGD CAP.
	** PROBLE	1S/SOLUT)	ONS/COMMENTS						
			SOME MINOR LE				UARY A	FTER TH	не тыо монтн
3/78	A		100.0	74.4	100.0				
	B System		98.8 99.4	74.4 74.4	98.8 99.4		744	744	739
	** PROBLEM	1S/SOLUT]	ONS/COMMENTS						
			ONE FORCED SH	IUTDOWN OCCUR	RED ON THE A	-SIDE SCRUBE	ING TR	AIN.	
4/78	A		92.7	99.9	92.7				
	В	100.0	100.0	100.0	100.0			700	
	SYSTEM		96.4	100.0	96.4		720	720	694
	** PROBLE	1S/SOLUTI	ONS/COMMENTS						
			A MINOR LEAK OVERHAUL/CLEA		NECESSARY AGA	IN AFTER THE	NOVEM	1AL-93E	IUAR Y
5/78	A		86.7	86.7	86.7				
	B System		96.2 91.5	98.1 92.4	96.2 91.5		744	744	680
	** PROBLE	1S/SOLUT]	ONS/COMMENTS						
			THERE WERE NO			PORTED. ONL	Y GENE	RAL MAI	INTENANCE WA
6/78	A	100.0	100.0	100. 0	100.0				
	B System		99.2 99.6	100.0	99.2		700	70.0	
	3131611		77.0	100.0	99.6		720	720	/1/
	VV 80001EN	40 400110							
	** PROBLET	1S/SOLUT]	ONS/COMMENTS	EDODIED NO M	44 105 SDOD! 5\				
		1S/SOLUT]	THE UTILITY F			S FOR THE MO	отн ог	JUNE.	
7/78	A		THE UTILITY F	99.4	99.4	S FOR THE MO	NTH OF	JUNE.	
7/78		15/SOLUT]	THE UTILITY F	99.4		S FOR THE MC	0NTH OF 744	JUNE.	742
7/78	A B System	100.0	THE UTILITY R 99.4 100.0	99.4 100.0	99.4 100.0	S FOR THE MC			742
7/78	A B System	100.0	THE UTILITY F 99.4 100.0 99.7	99.4 100.0 99.7	99.4 100.0 99.7		744	744	
7/78 8/78	A B SYSTEM ** PROBLEM	100.0	THE UTILITY F 99.4 100.0 99.7 CONS/COMMENTS ONLY ROUTINE 100.0	99.4 100.0 99.7 MAINTENANCE 100.0	99.4 100.0 99.7 WAS REQUIRED 100.0		744	744	
	A B SYSTEM ** PROBLEM	100.0 45/50LUT)	THE UTILITY F 99.4 100.0 99.7 CONS/COMMENTS ONLY ROUTINE	99.4 100.0 99.7 MAINTENANCE	99.4 100.0 99.7 WAS REQUIRED		744	744	<i>(</i> .
	A B SYSTEM ** PROBLEM A B SYSTEM	100.0 MS/SOLUTI	THE UTILITY F 99.4 100.0 99.7 CONS/COMMENTS ONLY ROUTINE 100.0 95.1	99.4 100.0 99.7 MAINTENANCE 100.0 95.1	99.4 100.0 99.7 WAS REQUIRED 100.0 95.1		744 ÆBER F	744 OR JULY	<i>(</i> .
	A B SYSTEM ** PROBLEM A B SYSTEM	100.0 MS/SOLUTI	THE UTILITY F 99.4 100.0 99.7 CONS/COMMENTS ONLY ROUTINE 100.0 95.1 97.6	99.4 100.0 99.7 MAINTENANCE 100.0 95.1 97.6	99.4 100.0 99.7 WAS REQUIRED 100.0 95.1 97.6	ON THE SCRU	744 ÆBER F1 744	744 OR JULY 744	726
	A B SYSTEM ** PROBLEM A B SYSTEM ** PROBLEM	100.0 MS/SOLUTI	THE UTILITY F 99.4 100.0 99.7 CONS/COMMENTS ONLY ROUTINE 100.0 95.1 97.6 CONS/COMMENTS REPAIRS WERE	99.4 100.0 99.7 MAINTENANCE 100.0 95.1 97.6	99.4 100.0 99.7 WAS REQUIRED 100.0 95.1 97.6	ON THE SCRU	744 ÆBER F1 744	744 OR JULY 744	726

PERIOD	MODULE AVAI	LABILITY		RELIABILITY	UTILIZATION					FGD HOURS	CAP.
	** PROBLEMS	/SOLUTIO	NS/COMMENTS								
				REPORTED NO	MAJOR PROBLEM	IS FOR	THE MO	октн ог	SEPTE	MBER.	
10/78			100.0	100.0	58.4						
	B SYSTEM		9 5.9 98 .0	100.0 100.0	56. 0 57.2			766	434	/ ₁ 2E	
	3131611		70.0	100.0	57.2			/44	434	425	
	** PROBLEMS	/SOLUTIO	NS/COMMENTS								
			ONLY ROUTINE	MAINTENANCE	WAS REQUIRED	он тн	E SCRU	JBBER I	и осто	BER.	
11/78		100.0		100.0	100.0						
	В		91.3	100.0 100.0	91.3						
	SYSTEM		95.7	100.0	95.7			72 0	720	688	
	** PROBLEMS	/SOLUTIO	NS/COMMENTS								
			THE UTILITY	REPORTED NO	MAJOR PROBLEM	S FOR	THE MO	отн ог	HOVEM	BER.	
12/78	A		88.1	88.1	88.1						
	В		85.6		85.6						
	SYSTEM		86.9	88.2	86.9			744	744	646	
	** PROBLEMS	/SOLUTIO	NS/COMMENTS								
			THE UTILITY LEMS DURING		THAT THE FGD	SYSTE	M EXPI	ERIENCE	D CONT	ROL PRO	OB-
1/79	A		99.1	99.1	99.1						
	В	100.0	100.0	100.0	100.0						
	SYSTEM		99.6	99.6	99.6			744	744	741	
2/79	Α	100.0	100.0	100.0	100.0						
	В	100.0	100.0	100.0	100.0						
	SYSTEM	100.0	100.0	100.0	100.0			672	672	672	
	** PROBLEMS	/SOLUTIO	NS/COMMENTS								
			THE UTILITY	REPORTED NO	MAJOR PROBLEM	S FOR	THE MO	онтн ог	FEBRU.	ARY.	
3/79	A		95.2	95.0	95.2						
	В	100. 0	100.0	100.0	100.0						
	SYSTEM		97.6	97.5	97.6			744	744	726	
	** PROBLEMS	/SOLUTIO	NS/COMMENTS								
		\$ \$ M	ECTIONALIZED TRUCTION AND	BUNDLES, WE MADE OF 316 ROCEDURES HA	CED PLUGGED RE ERE REPLACED W 6L SS. THE NE AS ADDED TO TH	ITH NE	W TUB! OF TI	ES OF S JBES AL	PLIT C	OIL CON	V- TER
4/79	A	100.0	100.0	100.0	100.0						
	В	100.0	100.0	100.0	100.0						

THE UTILITY REPORTED NO PROBLEMS FOR THE MONTH OF APRIL.

5/79 A 99.1 99.4 99.1

	MODULE AV	AILABILI	TY OPERABILITY	RELIABILITY	UTILIZATION		PER HOURS	BOILER HOURS	FGD HOURS	CAP. FACTOR
	B SYSTEM		44.1 71.6	44.1 71.8			744	744	533	
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			CORRODED DUCTWO	ORK ON MODUL	LE B FROM THE	TOWER TO TH	HE STAC	K WAS	REPLACE	D
			REPAIRS WERE M.	ADE TO THE N	10DULE B SCRU	BBER LINING.	•			
6/79	A		78.2	78.0	78.2					
	B System	100.0	100.0 89.1	100.0 89.0	100.0 89.1		720	720	642	
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			THE MODULE A A	BSORBER TOWE	ER MUNTERS PA	CKING WAS RE	EPLACED	DURIN	G JUNE.	
			EMERGENCY MAIN CHARGE HEADER.	TENANCE WAS	PERFORMED JU	NE 23 ON THE	MODUL	E A CO	MMON DI	s -
7/79	SYSTEM						744			
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			NO INFORMATION	WAS AVAILAE	SLE FOR THE M	ONTH OF JULY	۲.			
8/79			95.7	95.6	95.7					
	B System		95.7 95.7	95.7 95.7	95.7 95.7		744	744	712	
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			DURING AUGUST (GENERAL MAIN	TENANCE WAS	PERFORMED ON	1 THE F	LOODED	DISC	
9/79	SYSTEM						720			
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			INFORMATION WAS	S NOT AVAILA	ABLE FOR THE	MONTH OF SEF	TEMBER	٠		
10/79			97.8	100.0	45.0					
	B SYSTEM		94.3 96.1	98. 0 99. 0	43.3 44.2		744	342	328	
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			DURING OCTOBER	ROUTINE MAI	INTENANCE WAS	PERFORMED (ON THE	FGD SY	STEM.	
11/79			77.0		77.0					
	B System		98.5 87.8		98.5 87.8		720	720	632	
	A		94.0		94.0		, 2 4	, 20	032	
12/79			86.7		86.7					
12/79	В									
12/79	SYSTEM		90.4		90.4		744	744	672	
1/80			90.4 95.5		90.4 95.5		744	744	672	
12/ 7 9	SYSTEM						744	744	672	

2/80 A 100.0 100.0 100.0 100.0

PERIOD	MODULE			PERFORMAN RELIABILITY		% RE	MOVAL	PER			
	В		99.4		99.4						
	SYSTEM		99.7		99.7			696	696	694	92.1
3/80	A B		99.1 93.1		99.1 93.1						
	SYSTEM		96.1		96.1			744	744	715	88.6
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
		C	F NOVEMBER 1	AGES WERE REP 979 THROUGH M REPAIR OF THE	ARCH 1980.	SOME	SCHEDU				RIOD
4/80	A	100.0	100.0	100.0 100.0	100.0						
	B SYSTEM	100.0	100.0	100.0 100.0	100.0			720	720	720	82 8
		BLEMS/SOLUTIO		100.0	100.0			720	720	720	02.0
	~~ FRO			D PROBLEMS WE	DE REPORTED	FOR T	HE MON	TH OF	A PD T I		
E/00	A						1,5 1,5.1	0			
5/60	В	99.2	99.2	100.0 99.2 99.6	99.2						
	SYSTEM	99.6	99.6	99.6	99.6			744	744	741	87.6
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			THE B-MODULE FAN.	OUTAGE TIME I	N MAY WAS CA	USED	BY PRO	BLEMS I	WITH TH	E BOOS	TER
6/80	A B	100.0 99.3	80.7	100.0 99.1	68.7						
		99.3 99.7	84.2	99.1	74.6 71.7			720	613	516	67.5
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
				CHEDULED MAIN AGE TIME WAS		_					
				RELATED OUTAG WAS OUT OF SE				VALVE	MALFUN	CTIONE	o.
7/80				100.0							
	B SYSTEM	100.0 100.0	98.6 99.3	100.0 100.0	98.6 99.3			744	744	739	95.8
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
				M WAS AVAILAB PART OF THE M					MODULE	B WAS	HOT
8/80	SYSTEM							744			
9/80	SYSTEM							720			
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			DATA FOR THE PERSONNEL CHA	AUGUST AND SE NGES.	PTEMBER MONT	HS WE	RE NOT	AVAIL	ABLE DU	E TO	
10/80	SYSTEM							744			
11/80	SYSTEM							720			
12/80	SYSTEM							744			

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY HAS REPORTED THAT THE AVAILABILITY FIGURES FOR AUGUST THROUGH DECEMBER ARE NOT AVAILABLE AT THIS TIME.

DURING THE FOURTH QUARTER THE DUCTWORK DOWNSTREAM OF THE B TRAIN SCRUBBERS HAD TO BE REPLACED.

1/81	SYSTEM	744
2/81	SYSTEM	672
3/81	SYSTEM	744
4/81	SYSTEM	720
5/81	SYSTEM	744
6/81	SYSTEM	720
7/81	SYSTEM	744
8/81	SYSTEM	744
9/81	SYSTEM	720
10/81	SYSTEM	744
11/81	SYSTEM	72 0
12/81	SYSTEM	744
1/82	SYSTEM	744
2/82	SYSTEM	672
3/82	SYSTEM	744
4/82	SYSTEM	72 0
5/82	SYSTEM	744
6/82	SYSTEM	720
7/82	SYSTEM	744
8/82	SYSTEM	744
9/82	SYSTEM	720
10/82	SYSTEM	744
11/82	SYSTEM	720
12/82	SYSTEM	744
1/83	SYSTEM	744
2/83	SYSTEM	672
3/83	SYSTEM	744

PERIOD	MODULE	A	VA	I LAI	BILI	ΙΤΥ	01	PER	AB:	ILI	ΤY	RE	ELI	AB:	ILI	TY U	TIL	ΙZ	ATIO	ОИ	% S	RE 02	MO P	VAL ART	НС	ER URS	ВС	ILE	R	FGD		CAP.
	** PRO	ВL	EM	S/S	ວເຫ	rio	NS.	/cc	MM	ENT	'S																					
						I	NF	ORI	1AT	ION	ı W	AS	UN	iav.	AIL	ABLE	FO	₹ -	ГΗΕ	P	ERI	OD	OF	JAI	VUAF	Y 1	981	. то	M.	ARCH	1	983.
4/83	SYSTEM																									720						
5/83	SYSTEM	l																								744						
6/83	SYSTEM	l																								720						
	** PRO	BL	EM.	s/s	ורת	rio	NS.	/C0	MM	ENT	s																					
						I	NF	ORI	1AT	10I	1 M	AS	UN	łΑV.	AIL	ABLE	FO	₹ .	THE	P	ERI	OD	OF	JAI	YUAF	Y 1	981	ь то	JI	UNE :	198	33.
7/83	SYSTEM	ſ																								744						
8/83	SYSTEM	ı																								744						
9/83	SYSTEM	t																								720						
	** PRO	BL	EM.	S/S	օւՄ	TIC)NS	/C0	MMC	ENT	rs																					
						1	NF	ORI	1AT	10I	1 W.	AS	UΝ	VAV.	AIL	ABLE	FO	₽.	THE	T	HIR	0 0	UA	RTEI	R OF	: 19	83.					
10/83	SYSTEM	1																								744						
11/83	SYSTEM	1																								720						
12/83	SYSTEM	1																								744						
	** PRO	BL	٣٩.	5/5	OLU	TIC)NS	/00	MMC	ЕИП	rs																					
						1	NF	ORI	1AT	10I	4 M	AS	Uħ	۷A۷	AIL	ABLE	FO	R '	THE	F	OUR	тн	QU	ART	ER ()F 1	983	3.				
1/84	SYSTEM	1																								744						
2/84	SYSTEM	1																								696						
3/84	SYSTEM	1																								744						
4/84	SYSTEM	1																								720						
5/84	SYSTEM	1																								744	,					
6/84	SYSTEM	1																								720	1					
7/84	SYSTEM	1																								744						
8/84	SYSTEM	1																								744						
9/84	SYSTEM	1																								720	}					

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS NOT AVAILABLE FOR THE FIRST THREE QUARTERS OF 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

ARIZONA PUBLIC SERVICE COMPANY NAME PLANT NAME CHOLLA UNIT NUMBER JOSEPH CITY CITY STATE ARIZONA REGULATORY CLASSIFICATION 72. (.167 LB/MMBTU) 430. (1.000 LB/MMBTU) 344. (.800 LB/MMBTU) 615 PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW 285 GROSS UNIT GENERATING CAPACITY - MW NET UNIT GENERATING CAPACITY W/FGD - MW 235 250 NET UNIT GENERATING CAPACITY WO/FGD - MW EQUIVALENT SCRUBBED CAPACITY - MW 285 ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER COMBUSTION ENGINEERING BOILER TYPE PULVERIZED COAL BOILER SERVICE LOAD BASE DESIGN BOILER FLUE GAS FLOW - CU.M/S 519.09 (1100000 ACFM) 142.2 (288 F) 168. (550 FT) BOILER FLUE GAS TEMPERATURE - C STACK HEIGHT M CONCRETE 4.5 STACK SHELL STACK TOP DIAMETER - M (14.7 FT) ** FUEL DATA FUEL TYPE COAL FUEL GRADE BITUMINOUS AVERAGE HEAT CONTENT - J/G 23609. (10150 BTU/LB) RANGE HEAT CONTENT - BTU/LB 9650-10600 AVERAGE ASH CONTENT - % 13.50 RANGE ASH CONTENT - % 9.7-22.5 AVERAGE MOISTURE CONTENT % 15.00 RANGE MOISTURE CONTENT - % AVERAGE SULFUR CONTENT - % .50 RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % .02 RANGE CHLORIDE CONTENT - % 0.01-0.04 *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER NUMBER OF SPARES Ω TYPE CYCLONE 259.5 (550000 ACFM) 137.8 (280 E) SUPPLIER RESEARCH-COTTRELL INLET FLUE GAS CAPACITY CU.M/S INLET FLUE GAS TEMPERATURE - C PARTICLE REMOVAL EFFICENCY -% 70.0 ** ESP NUMBER n TYPE NONE ** PARTICLE SCRUBBER NUMBER NUMBER OF SPARES 1 GENERIC TYPE VENTURI TOWER SPECIFIC TYPE VARIABLE-THROAT/BOTTOM-ENTRY LIQUID DISTRIBUTION TRADE NAME/COMMON NAME FLOODED DISC SCRUBBER SUPPLIER RESEARCH-COTTRELL DIMENSIONS - FT 6.0 DIA X 45.0 SHELL GENERIC MATERIAL CARBON STEEL SHELL SPECIFIC MATERIAL AISI 1110 LINER GENERIC MATERIAL ORGANIC LINER SPECIFIC MATERIAL MAT-REINFORCED EPOXY GAS CONTACTING DEVICE TYPE NONE NUMBER OF CONTACTING ZONES 1 LIQUID RECIRCULATION RATE - LITER/S 617.4 (9800 GPM)

```
L/G RATIO
               LITER/CU.M
                                                   3.3
                                                              (25.0 GAL/1000ACF)
                                               ABSORBER SLURRY
    PH CONTROL ADDITIVE
                                               5.7 (23.0 IN-H2O)
    PRESSURE DROP - KPA
                                                              ( 392000 ACFM)
    INLET GAS FLOW RATE - CU.M/S
                                                 185.0
                                                              ( 280 F)
    INLET GAS TEMPERATURE - C
                                                 137.8
    PARTICLE REMOVAL EFFICIENCY - %
                                                  99.0
*** FGD SYSTEM
 ** GENERAL DATA
    SALEABLE PRODUCT/THROWAWAY PRODUCT
                                               THROWAWAY PRODUCT
    SO2 REMOVAL MODE
                                               WET SCRUBBING
    PROCESS TYPE
                                               LIMESTONE
    PROCESS ADDITIVES
                                               NONE
    SYSTEM SUPPLIER
                                               RESEARCH-COTTRELL
    A-E FIRM
                                               EBASCO
                                               FULL SCALE
    DEVELOPMENT LEVEL
    NEW/RETROFIT
                                               NEW
    UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.70
    UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                  75.00
     ENERGY CONSUMPTION - %
                                                   5.3
     CURRENT STATUS
                                                1
                                                6/78
     COMMERCIAL START-UP
     INITIAL START-UP
                                                4/78
     CONTRACT AWARDED
                                               12/74
 ** DESIGN AND OPERATING PARAMETERS
     OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                 40.0
 ** QUENCHER/PRESATURATOR
     NUMBER
                                                 0
 ** ABSORBER
                                                 4
     NUMBER
     NUMBER OF SPARES
                                                1
     GENERIC TYPE
                                                COMBINATION TOWER
     SPECIFIC TYPE
                                                SPRAY/PACKED
     TRADE NAME/COMMON TYPE
                                               N/A
     SUPPLIER
                                                RESEARCH-COTTRELL
                                               22.0 DTA X 70.0
     DIMENSIONS FT
     SHELL GENERIC MATERIAL
                                                CARBON STEEL
                                               AISI 1110
     SHELL SPECIFIC MATERIAL
     SHELL MATERIAL TRADE NAME/COMMON TYPE
                                                N/A
     LINER GENERIC MATERIAL
                                               OPGANIC
     LINER SPECIFIC MATERIAL
                                               MAT-REINFORCED EPOXY; GLASS FLAKE-FILLED POLYEST
                                               COROLINE 505AR; FLAKELINE 103
     LINER MATERIAL TRADE NAME/COMMON TYPE
     GAS CONTACTING DEVICE TYPE
                                                VERTICAL CROSS CHANNEL FIXED GRID PACKING
     NUMBER OF CONTACTING ZONES
                                                2
     LIQUID RECIRCULATION RATE - LITER/S
                                                1210.
                                                              (19200 GPM)
                                                   6.5
     L/G RATIO - L/CU.M
                                                              ( 48.9 GAL/1000 ACF)
     SUPERFICAL GAS VELOCITY - M/SEC
                                                   3.0
                                                              ( 10.0 FT/S)
                                                              ( 392000 ACFM)
     INLET GAS FLOW CU. M/S
                                                 184.98
                                                  50.0
                                                              ( 122 F)
     INLET GAS TEMPERATURE - C
     SO2 REMOVAL EFFICIENCY - %
                                                   98.0
     PARTICLE REMOVAL EFFICENCY - %
                                                   99.0
 ** MIST ELIMINATOR
                                                PRIMARY COLLECTOR
     PRE-MIST ELIMINATOR/MIST ELIMINATOR
     NUMBER PER SYSTEM
                                                 4
     NUMBER OF SPARES PER SYSTEM
                                                1
     NUMBER PER MODULE
                                                1
     GENERIC TYPE
                                                CYCLONIC
                                                CYCLONIC SEPARATOR
     SPECIFIC TYPE
     TRADE NAME/COMMON TYPE
                                                CYCLONIC TOWER
                                                VERTICAL
     CONFIGURATION
     NUMBER OF STAGES
                                               STAINLESS STEEL
     CONSTRUCTION MATERIAL GENERIC TYPE
     CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               AUSTENITIC
     WASH WATER SOURCE
                                                NONE
     WASH FREQUENCY
                                                N/A
```

GENERIC TYPE

```
** REHEATER
                                                 4
   NUMBER
                                                 1
   NUMBER OF SPARES
                                                1
   NUMBER PER MODULE
   GENERIC TYPE
                                                IN-LINE
                                               STEAM
   SPECIFIC TYPE
   TRADE NAME/COMMON TYPE
                                               BARE TUBE
                                               TOP OF THE ABSORBER
    LOCATION
                                                              ( 40 F)
                                                  22.2
    TEMPERATURE INCREASE - C
                                                                 121 F}
    INLET FLUE GAS TEMPERATURE - C
                                                   49.4
                                                               ( 160 F)
                                                   71.1
    OUTLET FLUE GAS TEMPERATURE - C
   NUMBER OF HEAT EXCHANGER BANKS
                                                   3
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               HIGH ALLOY
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               NICKEL BASE/CHROMIUM-IRON-MOLYBDENUM
** FANS
   NUMBER
                                                 2
                                                CENTRIFUGAL
   DESIGN
    FUNCTION
                                               UNIT
                                                FORCED DRAFT
    APPLICATION
                                               DRY
    SERVICE
    FLUE GAS TEMPERATURE - C
                                                 137.8
                                                               ( 280 F)
                                               NR
    CONSTRUCTION MATERIAL GENERIC TYPE
** FANS
    NUMBER
    DESIGN
                                               CENTRIFUGAL
    FUNCTION
                                               BOOSTER
    APPLICATION
                                               INDUCED DRAFT
    SERVICE
    FLUE GAS TEMPERATURE C
                                                              ( 160 F)
                                                   71.1
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                ORGANIC; CARBON STEEL [HOUSING]; STAINLESS STEEL
** DAMPERS
   NUMBER
                                                SHUT-OFF
    FUNCTION
    GENERIC TYPE
                                                GUILLOTINE
    SPECIFIC TYPE
                                                NR
    MANUFACTURER
                                               MOSSER
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL
    LINER GENERIC MATERIAL TYPE
                                                STAINLESS STEEL
    LINER SPECIFIC MATERIAL TYPE
                                                AUSTENITIC
** DAMPERS
    NUMBER
                                                 4
    FUNCTION
                                                CONTROL
    GENERIC TYPE
                                                LOUVER
    SPECIFIC TYPE
                                                NR
    MANUFACTURER
                                                MOSSER
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                STAINLESS STEEL
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                AUSTENITIC
    LINER GENERIC MATERIAL TYPE
                                                NONE
    LINER SPECIFIC MATERIAL TYPE
                                                N/A
** DAMPERS
    NUMBER
                                                 2
    FUNCTION
                                                CONTROL
    GENERIC TYPE
                                                LOUVER
    MANUFACTURER
                                                MOSSER
** DAMPERS
    NUMBER
                                                 4
    FUNCTION
                                                CONTROL
    GENERIC TYPE
                                                LOUVER
   MANUFACTURER
                                                MOSSER
** DAMPERS
   NUMBER
                                                 4
    FUNCTION
                                                SHUT-OFF
```

LOUVER

MANUFACTURER MOSSER

** DUCTWORK

LOCATION INLET SHELL GENERIC MATERIAL TYPE CARBON STEEL AISI 1110 SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A

** DUCTWORK

LOCATION OUTLET SHELL GENERIC MATERIAL TYPE CARBON STEEL SHELL SPECIFIC MATERIAL TYPE AISI 1110 LINER GENERIC MATERIAL TYPE ORGANIC; ORGANIC

LINER SPECIFIC MATERIAL TYPE GLASS FLAKE-FILLED POLYESTER; INERT FLAKE-FILLED

** DUCTWORK

LOCATION **BYPASS** SHELL GENERIC MATERIAL TYPE CARBON STEEL SHELL SPECIFIC MATERIAL TYPE AISI 1110 LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A

** REAGENT PREPARATION EQUIPMENT

FUNCTION WET BALL MILL COMPARTMENTED DEVICE DEVICE TYPE ΝR

MANUFACTURER KENNEDY VAN SAUN 2

NUMBER

FULL LOAD DRY FEED CAPACITY - M.TONS/HR 6.4 (7 TPH) PRODUCT QUALITY - % SOLIDS 25.0

** TANKS

SERVICE NUMBER ----ABSORBER FEED 2 REAGENT FEED **** MILL SLURRY SUMP **** SCRUBBER RECYCLE 4 SLUDGE STORAGE ***

** PUMPS

SERVICE NUMBER SCRUBBER RECIRCULATION 12 ABSORBER RECIRCULATION 8 MILL SLURRY SUMP **** **** REAGENT FEED MIST ELIMINATOR WASH ****

*** SLUDGE

MOISTURE CONTENT - % TOTAL FREE WATER 35.0

** TREATMENT

METHOD STABILIZATION DEVICE NR PROPRIETARY PROCESS NONE INLET QUALITY - % 15.0

** DISPOSAL

NATURE FINAL POND TYPE ON-SITE LOCATION PIPELINE SITE TRANSPORTATION METHOD SITE TREATMENT NONE

** PROCESS CONTROL AND INSTRUMENTATION

PROCESS STREAM SCRUBBER AND ABSORBER HOLD TANK CHEMICAL PARAMETERS PH

UTILITY FGD SURVEY: OCTOBER 1983 - SEPTEMBER 1984

ARIZONA PUBLIC SERVICE: CHOLLA 2 (CONT.)

CONTROL LEVELS PH 4.8-5.2 IN SCRUBBER HOLD TANK; 5.9-6.2 IN ABS

** WATER BALANCE

WATER LOOP TYPE OPEN

MAKEUP WATER ADDITION - LITERS/S 7.6 (120 GPM)

** CHEMICALS AND CONSUMPTION

FUNCTION ABSORBENT
NAME LIMESTONE
POINT OF ADDITION BALL MILL

** FGD SPARE CAPACITY INDICES

 SCRUBBER - %
 33.3

 ABSORBER - %
 33.3

** FGD SPARE COMPONENT INDICES

SCRUBBER 1.0 ABSORBER 1.0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

502 PART. HOURS HOURS FACTOR

4/78 SYSTEM 720

5/78 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

INITIAL SCRUBBING OPERATIONS BEGAN IN APRIL 1978. THE SCRUBBER REPORTEDLY OPERATES MOST OF THE TIME, HOWEVER, SOME PROBLEMS HAVE OCCURRED WITH VIBRATIONS THROUGHOUT THE SYSTEM.

THE EPA HAS RECENTLY GRANTED THE UTILITY AN EXTENSION FOR COMPLIANCE. FULL COMMERCIAL OPERATIONS ARE EXPECTED TO BEGIN SOMETIME AFTER MIDAUGUST. THE COMPLIANCE TEST WILL BE COMPLETED BY AUGUST 15. THE UTILITY EXPECTS TO HAVE THE FGD SYSTEM SHAKEDOWN PROBLEMS CLEARED UP BY THEN.

6/78 SYSTEM 720

7/78 SYSTEM **744**

** PROBLEMS/SOLUTIONS/COMMENTS

SHAKEDOWN/DEBUGGING OPERATIONS ARE CONTINUING.

THE SLURRY RECYCLE PIPING HAS EXPERIENCED CONTINUAL VIBRATION PROBLEMS. THE CONTRACTOR HAS BEEN INJECTING NITROGEN GAS INTO THE LINES TO DAMPEN THE VIBRATIONS (AIR WAS NOT USED BECAUSE THE SULFITE WOULD BE OXIDIZED TO SULFATE AND RESULT IN SCALE FORMATION).

THE CORROSION RESISTANT COATING IN THE DOWNCOMER AREA IN ONE OF THE ABSORBER MODULES HAS BEEN PEELING AWAY.

8/78 SYSTEM 744

9/78 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE SLURRY RECYCLE SYSTEM COMPONENTS ARE STILL EXPERIENCING RESONANT VIBRATIONS.

THE COMPLIANCE TEST WAS PERFORMED THE WEEK OF AUGUST 7. ALTHOUGH OFFICIAL WORD HAS NOT BEEN RECEIVED BY THE UTILITY IT APPEARS THAT THE UNIT IS IN COMPLIANCE WITH RESPECT TO SO2, PARTICULATE MATTER, OPACITY AND NOX.

SHAKEDOWN/DEBUGGING OPERATIONS ARE CONTINUING.

				PERFORMAN	ICE DATA							
PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% REI	MOVAL	PER	BOILER	FGD	CAP.	
						\$02	PART.	HOURS	HOURS	HOURS	FACTOR	
10/78	SYSTEM							744				
11/78	SYSTEM							720				

** PROBLEMS/SOLUTIONS/COMMENTS

SHAKEDOWN DEBUGGING OPERATIONS ARE CONTINUING. SOME SCRUBBER COMPONENTS ARE STILL MANNED BY BECHTEL STAFF, ARIZONA PUBLIC SERVICE PERSONNEL ARE OPERATING MOST OF THE SYSTEM AT THIS TIME.

12/78 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

DECEMBER-JANUARY INFORMATION IS UNAVAILABLE AT THIS TIME FOR CHOLLA 2. THE UTILITY REPORTED THAT IT WOULD SOON BE KEEPING PERFORMANCE RECORDS.

		THE	UTILITY	REPORTED	THAT	ΙT	MOULD	SOON	BE	KEEPING	PERFOR
1/79	SYSTEM										744
2/79	SYSTEM										672
3/79	SYSTEM										744
4/79	SYSTEM										720
5/79	SYSTEM										744
6/79	SYSTEM										720
7/79	SYSTEM										744
8/79	SYSTEM										744
9/79	SYSTEM										720
10/79	SYSTEM										744
11/79	SYSTEM										720
12/79	SYSTEM										744
1/80	SYSTEM										744
2/80	SYSTEM										696
3/80	SYSTEM										744
4/80	SYSTEM										720
5/80	SYSTEM										744
6/80	SYSTEM										720
7/80	SYSTEM										744
8/80	SYSTEM										744
9/80	SYSTEM										720
10/80	SYSTEM										744
11/80	SYSTEM										720
12/80	SYSTEM										744

				PERFORMAN	ICE DATA						
PERIOD		AVAILABILITY				\$02	PART.	HOURS	HOURS	HOURS	FACTOR
	SYSTEM							744			
	SYSTEM							672			
	SYSTEM							744			
	SYSTEM							720			
	SYSTEM							744			
	SYSTEM							720			
	SYSTEM							744			
	SYSTEM							744			
	SYSTEM							720			
	SYSTEM							744			
	SYSTEM							720			
	SYSTEM							744			
	SYSTEM							744			
	SYSTEM							672			
	SYSTEM							744			
	SYSTEM							720			
	SYSTEM							720			
	SYSTEM							720			
	SYSTEM							744			
	SYSTEM							744			
	SYSTEM							720			
	SYSTEM							744			
	SYSTEM							720			
	SYSTEM							744			
	SYSTEM							744			
	SYSTEM							672			
5/83	SYSTEM							744			
	** PROB	LEMS/SOLUTION									
		IN	FORMATION WA	S UNAVAILABL	E FOR THE P	ERIOD O	F JANU	ARY 19	79 TO M	ARCH 1	983.
	SYSTEM							720			
	SYSTEM							744			
6/83	SYSTEM							720			

PERFORMANCE DATA		 	
PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION			
	SO2 PART.		

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE PERIOD OF JANUARY 1979 TO JUNE 1983.

7/83	SYSTEM	744
8/83	SYSTEM	744
9/83	SYSTEM	720

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE THIRD QUARTER OF 1983.

10/83	SYSTEM	744
11/83	SYSTEM	720
12/83	SYSTEM	744

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE FOURTH QUARTER OF 1983.

1/84	SYSTEM	744
2/84	SYSTEM	696
3/84	SYSTEM	744
4/84	SYSTEM	720
5/84	SYSTEM	744
6/84	SYSTEM	720
7/84	SYSTEM	744
8/84	SYSTEM	744
9/84	SYSTEM	720

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS NOT AVAILABLE FOR THE FIRST THREE QUARTERS OF 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COMPANY NAME PLANT NAME UNIT NUMBER CITY STATE REGULATORY CLASSIFICATION PARTICULATE EMISSION LIMITA SO2 EMISSION LIMITATION N NOX EMISSION LIMITATION - N NET PLANT GENERATING CAPACI GROSS UNIT GENERATING CAPACIT NET UNIT GENERATING CAPACIT NET UNIT GENERATING CAPACIT EQUIVALENT SCRUBBED CAPACIT	G/J TY - MW ITY - MW Y W/FGD - MW Y WO/FGD - MW	ARIZONA PUBLIC CHOLLA 4 JOSEPH CITY ARIZONA A ****** ****** 965 375 375 350 495 126	SERVICE (****** LB/MMBTU) (****** LB/MMBTU) (****** LB/MMBTU)
** UNIT DATA BOILER AND BOILER SUPPLIER BOILER TYPE BOILER SERVICE LOAD DESIGN BOILER FLUE GAS BOILER FLUE GAS TEMPER STACK HEIGHT M STACK SHELL STACK TOP DIAMETER - M	FLOW - CU.M/S ATURE C	****** CONCRETE	
** FUEL DATA FUEL TYPE FUEL GRADE AVERAGE HEAT CONTENT - B AVERAGE ASH CONTENT - R ANGE ASH CONTENT - R AVERAGE MOISTURE CONTE RANGE MOISTURE CONTENT AVERAGE SULFUR CONTENT RANGE SULFUR CONTENT AVERAGE CHLORIDE CONTE RANGE CHLORIDE CONTENT	TU/LB % NT - %	COAL ***** 23609. 13.50 ***** 15.00 ***** .50 0.4-1.0 .02 0.01-0.04	(10150 BTU/LB) *****
*** PARTICLE CONTROL			
** ESP NUMBER		1	
** PARTICLE SCRUBBER NUMBER GENERIC TYPE SPECIFIC TYPE TRADE NAME/COMMON NAME SHELL GENERIC MATERIAL SHELL SPECIFIC MATERIAL LINER GENERIC MATERIAL LINER SPECIFIC MATERIAL GAS CONTACTING DEVICE	L	0 NONE N/A N/A N/A N/A N/A N/A	
*** FGD SYSTEM			
** GENERAL DATA SALEABLE PRODUCT/THROW SO2 REMOVAL MODE PROCESS TYPE SYSTEM SUPPLIER A-E FIRM DEVELOPMENT LEVEL NEW/RETROFIT UNIT DESIGN SO2 REMOVA CUPRENT STATUS COMMERCIAL START-UP INITIAL START-UP		THROWAWAY PROD WET SCRUBBING LIMESTONE RESEARCH-COTTR EBASCO FULL SCALE NEW 95.00 1 6/81 3/81	

CONTRACT AWARDED 10/77

** DESIGN AND OPERATING PARAMETERS

** QUENCHER/PRESATURATOR

CONSTRUCTION MATERIAL GENERIC TYPE NR
CONSTRUCTION MATERIAL SPECIFIC TYPE NR

** ABSORBER

NUMBER GENERIC TYPE COMBINATION TOWER SPECIFIC TYPE SPRAY/PACKED TRADE NAME/COMMON TYPE N/A SHELL GENERIC MATERIAL NR SHELL SPECIFIC MATERIAL NR SHELL MATERIAL TRADE NAME/COMMON TYPE NR LINER GENERIC MATERIAL ND LINER SPECIFIC MATERIAL NR LINER MATERIAL TRADE NAME/COMMON TYPE NR SO2 REMOVAL EFFICIENCY - % 95.0

** MIST ELIMINATOR

PRE-MIST ELIMINATOR/MIST ELIMINATOR
GENERIC TYPE
SPECIFIC TYPE
TRADE NAME/COMMON TYPE
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
NR
CONSTRUCTION MATERIAL SPECIFIC TYPE
NR

** REHEATER

GENERIC TYPE NR
SPECIFIC TYPE NR
TRADE NAME/COMMON TYPE NR
CONSTRUCTION MATERIAL GENERIC TYPE NR
CONSTRUCTION MATERIAL SPECIFIC TYPE NR

** FANS

DESIGN CENTRIFUGAL
FUNCTION NR
APPLICATION FORCED DRAFT
SERVICE DRY
CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL

** DAMPERS

FUNCTION NR
GENERIC TYPE NR
SPECIFIC TYPE NR
CONSTRUCTION MATERIAL GENERIC TYPE NR
CONSTRUCTION MATERIAL SPECIFIC TYPE NR
LINER GENERIC MATERIAL TYPE NR
LINER SPECIFIC MATERIAL TYPE NR

** DUCTWORK

SHELL GENERIC MATERIAL TYPE NR
SHELL SPECIFIC MATERIAL TYPE NR
LINER GENERIC MATERIAL TYPE NR
LINER SPECIFIC MATERIAL TYPE NR

** REAGENT PREPARATION EQUIPMENT

FUNCTION WET BALL MILL
DEVICE COMPARTMENTED
DEVICE TYPE NR

** TANKS

SERVICE NUMBER

UTILITY FGD SURVEY: OCTOBER 1983 SEPTEMBER 1984

ARIZONA PUBLIC SERVICE: CHOLLA 4 (CONT.)

** PUMPS SERVICE NUMBER _____ -----*** ** SOLIDS CONCENTRATING/DEWATERING NA DEVICE *** SLUDGE ** TREATMENT NA METHOD DEVICE NA PROPRIETARY PROCESS NΑ ** DISPOSAL FINAL NATURE POND TYPE LOCATION ON-SITE NONE SITE TREATMENT

ABSORBER % .0

** FGD SPARE COMPONENT INDICES
ABSORBER .0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

** FGD SPARE CAPACITY INDICES

3/81 SYSTEM

IN MARCH 1981 THE FGD SYSTEM COMMENCED OPERATIONS. THE SYSTEM OPERATED FOR APPROXIMATELY ONE WEEK BEFORE BEING TAKEN OFF LINE FOR A BEARING INSPECTION.

744

4/81	SYSTEM	720
5/81	SYSTEM	744
6/81	SYSTEM	720
7/81	SYSTEM	744
8/81	SYSTEM	744
9/81	SYSTEM	720
10/81	SYSTEM	744
11/81	SYSTEM	72 0
12/81	SYSTEM	744
1/82	SYSTEM	744
2/82	SYSTEM	672
3/82	SYSTEM	744
4/82	SYSTEM	720
5/82	SYSTEM	720

		AVAILABILITY										
PERTOD	1100000	AVAILABILITI					502	PART.	HOURS		HOURS	FACTOR
6/82	SYSTEM								720			
	SYSTEM								744			
	SYSTEM								744			
9/82	SYSTEM								720			
10/82	SYSTEM								744			
11/82	SYSTEM								720			
12/82	SYSTEM								744			
1/83	SYSTEM								744			
2/83	SYSTEM								672			
3/83	SYSTEM								744			
	** PROE	BLEMS/SOLUTION	NS/COMMENTS									
		I	NFORMATION WA	AS UNAVAILAB	LE FOR T	не ре	RIOD (DF APR	IL 198	1 TO MAI	RCH 198	33.
4/83	SYSTEM								720			
5/83	SYSTEM								744			
6/83	SYSTEM								72 0			
	** PRO	BLEMS/SOLUTIO										
			NFORMATION WA	AS UNAVAILAB	LE FOR T	HE PE	RIOD	OF APR		ו דס טעו	NE 198	3.
	SYSTEM								744			
	SYSTEM								744			
9/83	SYSTEM		NC /COMMENTS						720			
	** PRU	BLEMS/SOLUTIO	NEORMATION WA	AS INVAVATIAR	IF FOD T	WE TW	ום חפדו	IIADTED	OF 19	A 7		
10/83	SYSTEM		IN ORNATION A	AS CHAVAILAD	LL TOR I	112 11	IIKD 4	DARTER	744	٠,٠		
	SYSTEM								720			
	SYSTEM								744			
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS									
		I	NFORMATION W	AS UNAVAILAB	LE FOR T	HE FO	HTAU	QUARTE	R OF 1	983.		
1/84	SYSTEM								744			
2/84	SYSTEM								696			
47.04												
	SYSTEM								744			
3/84	SYSTEM SYSTEM								744 720			

UTILITY FGD SURVEY: OCTOBER 1983 - SEPTEMBER 1984

ARIZONA PUBLIC SERVICE: CHOLLA 4 (CONT.)

PERFORMANCE DATA	
PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER	FGD CAP.
SO2 PART, HOURS HOURS H	
6/84 SYSTEM 720	
7/84 SYSTEM 744	
8/84 SYSTEM 744	
9/84 SYSTEM 720	

^{**} PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS NOT AVAILABLE FOR THE FIRST THREE QUARTERS OF 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

ARIZONA PUBLIC SERVICE COMPANY NAME FOUR CORNERS PLANT NAME UNIT NUMBER FRUITLAND CITY NEW MEXICO STATE REGULATORY CLASSIFICATION 21. (.050 LB/MMBTU) 365. (.850 LB/MMBTU) 301. (.700 LB/MMBTU) 2085 С PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J HET PLANT GENERATING CAPACITY - MW 195 170 GROSS UNIT GENERATING CAPACITY - MW NET UNIT GENERATING CAPACITY W/FGD - MW NET UNIT GENERATING CAPACITY WO/FGD - MW 175 EQUIVALENT SCRUBBED CAPACITY - MW 195 ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER RILEY STOKER BOILER TYPE PULVERIZED COAL BOILER SERVICE LOAD BASE DESIGN BOILER FLUE GAS FLOW - CU.M/S BOILER FLUE GAS TEMPERATURE - C 384.13 (814000 ACFM) 171.1 (340 F) 76. (250 FT) STACK HEIGHT - M CONCRETE 5.3 STACK SHELL STACK TOP DIAMETER - M (17.5 FT) ** FUEL DATA FUEL TYPE COAL FUEL GRADE SUBBITUMINOUS AVERAGE HEAT CONTENT - J/G 20004. (8600 BTU/LB) RANGE HEAT CONTENT - BTU/LB 8500-9100 AVERAGE ASH CONTENT - % 22.00 RANGE ASH CONTENT - % 19-25 AVERAGE MOISTURE CONTENT % 10.80 RANGE MOISTURE CONTENT - % 8.5-13.4 AVERAGE SULFUR CONTENT - % .5-1.3 .0: RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % .03 RANGE CHLORIDE CONTENT - % .01-.06 *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER 0 TYPE NONE ** ESP NUMBER 0 TYPE NONE *** FGD SYSTEM ** GENERAL DATA SALEABLE PRODUCT/THROWAWAY PRODUCT THROWAWAY PRODUCT SO2 REMOVAL MODE WET SCRUBBING PROCESS TYPE LIME/ALKALINE FLYASH PROCESS ADDITIVES NONE SYSTEM SUPPLIER GE ENVIRONMENTAL SERVICES A-E FIRM IN-HOUSE DEVELOPMENT LEVEL FULL SCALE NEW/RETROFIT RETROFIT UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.50 50.00 UNIT DESIGN SO2 REMOVAL EFFICIENCY % ENERGY CONSUMPTION - X 2.6 CURRENT STATUS 11/79 COMMERCIAL START-UP INITIAL START-UP 11/79 CONTRACT AWARDED 0/78

ARIZONA PUBLIC SERVICE: FOUR CORNERS 1 (CONT.)

```
** DESIGN AND OPERATING PARAMETERS
   DESIGN COAL SULFER CONTENT - %
                                                  1.30
                                              19771.0
                                                           ( 8500 BTU/LB)
   DESIGN COAL HEAT CONTENT - J/G
   DESIGN COAL ASH CONTENT - %
                                                25.00
   DESIGN MOISTURE CONTENT - %
                                                 13.40
   DESIGN CHLORIDE CONTENT - %
                                                  .06
                                                520.2
                                                           ( 5600 SQ FT)
    SPACE REQUIREMENTS - SQ M
    OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                200.0
** QUENCHER/PRESATURATOR
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              NR
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              NR
** ABSORBER
   NUMBER
                                               2
   NUMBER OF SPARES
                                               0
                                              VENTURI TOWER
   GENERIC TYPE
                                              VARIABLE-THROAT/TOP-ENTRY PLUMB BOB
    SPECIFIC TYPE
    TRADE NAME/COMMON TYPE
                                              N/A
    DIMENSIONS - FT
                                              25 DIA
    SHELL GENERIC MATERIAL
                                              CARBON STEEL
    SHELL SPECIFIC MATERIAL
                                              AISI 1110
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                              N/A
    LINER GENERIC MATERIAL
                                              ORGANIC
    LINER SPECIFIC MATERIAL
                                              GLASS FLAKE-FILLED POLYESTER
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                              FLAKELINE 103
    GAS CONTACTING DEVICE TYPE
                                              VENTURI THROAT [TANGENTIAL NOZZLES AT TOP & AT S
   NUMBER OF CONTACTING ZONES
                                               1
    LIQUID RECIRCULATION RATE LITER/S
                                               630.
                                                            (10000 GPM)
    L/G RATIO L/CU.M
                                                            ( 24.0 GAL/1000 ACF)
                                                  3.2
    GAS-SIDE PRESSURE DROP - KPA
                                                            (10.0 IN-H20)
                                                  2.5
    INLET GAS FLOH - CU. M/S
                                                192.06
                                                            ( 407000 ACFM)
    INLET GAS TEMPERATURE - C
                                               171.1
                                                            ( 340 F)
    SO2 REMOVAL EFFICIENCY - %
                                                 67.5
    PARTICLE REMOVAL EFFICENCY %
                                                 99.5
** MIST ELIMINATOR
    PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                             PRIMARY COLLECTOR
    NUMBER PER SYSTEM
    NUMBER OF SPARES PER SYSTEM
                                               ٥
    NUMBER PER MODULE
                                               1
    GENERIC TYPE
                                              IMPINGEMENT
    SPECIFIC TYPE
                                              BAFFLE
    TRADE NAME/COMMON TYPE
                                              CLOSED VANE
    CONFIGURATION
                                              HORIZONTAL
    NUMBER OF STAGES
                                                 1
    NUMBER OF PASSES PER STAGE
                                                  6
    CONSTRUCTION MATERIAL GENERIC TYPE
                                             ORGANIC
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                             FIBER-REINFORCED POLYESTER
    WASH WATER SOURCE
                                              FRESH [FROM LAKE]
    WASH FREQUENCY
                                              ONCE PER SHIFT
** REHEATER
   NUMBER
                                               0
    GENERIC TYPE
                                              NONE
    SPECIFIC TYPE
                                              N/A
    TRADE NAME/COMMON TYPE
                                              N/A
    CONSTRUCTION MATERIAL GENERIC TYPE
                                              NONE
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              N/A
** FANS
   NUMBER
                                               2
    NUMBER OF SPARES
                                               ٥
    DESIGN
                                              CENTRIFUGAL
    SUPPLIER
                                              AMERICAN STANDARD
    FUNCTION
                                              UNTT
    APPLICATION
                                              INDUCED DRAFT
    SERVICE
                                              WET
    FLUE GAS FLOH RATE CU.M/S
                                              259.54
                                                           ( 550000 ACFM)
```

51.7

(125 F)

FLUE GAS TEMPERATURE - C

ARIZONA PUBLIC SERVICE: FOUR CORNERS 1 (CONT.)	
CONSTRUCTION MATERIAL GENERIC TYPE	HIGH ALLOY
** DAMPERS NUMBER FUNCTION GENERIC TYPE SPECIFIC TYPE MANUFACTURER SERVICE CONDITIONS CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	2 CONTROL LOUVER PARALLEL BLADE MULTILOUVER AMERICAN STANDARD 120-130 F STAINLESS STEEL AUSTENITIC NONE N/A
** DAMPERS NUMBER FUNCTION GENERIC TYPE SPECIFIC TYPE MANUFACTURER SERVICE CONDITIONS CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	1 SHUT-OFF GUILLOTINE NR NR NR CARBON STEEL AISI 1110 NONE N/A
** DUCTWORK LOCATION CONFIGURATION DIMENSIONS SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	INLET CIRCULAR 14 DIA X 90 FT CARBON STEEL ASTM A-283 NONE N/A
** DUCTWORK LOCATION CONFIGURATION DIMENSIONS SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	OUTLET IME TO STACK! RECTANGULAR 12 X 12 X 50 FT CARBON STEEL ASTM A-283 STAINLESS STEEL AUSTENITIC
** REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE DEVICE TYPE MANUFACTURER NUMBER NUMBER NUMBER OF SPARES FULL LOAD DRY FEED CAPACITY - M.TONS/HR PRODUCT QUALITY - % SOLIDS	SLAKER NR NR JOY 1 0 13.6 (15 TPH)
** REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE DEVICE TYPE MANUFACTURER NUMBER NUMBER OF SPARES	WET BALL MILL NR NR KENNEDY VAN SAUN 1 0
** TANKS SERVICE BLEED STREAM RECYCLE MAKEUP WATER RETURN TRANSFER LIME SLURRY	NUMBER 1 2 1 1 4

13-91

ARIZONA PUBLIC SERVICE: FOUR CORNERS 1 (CONT.)

```
** PUMPS
                                               NUMBER
    SERVICE
    RECYCLE
    RECYCLE [STANDBY]
    BLEED STREAM TANK
                                                  4
    THICKENER UNDERFLOW
                                                  2
    LIME SLURRY TRANSFER
    RETURN WATER
                                                  2
                                               ****
    SERVICE WATER
                                               ****
    ME WATER
** SOLIDS CONCENTRATING/DEWATERING
    DEVICE
                                               THICKENER
                                                1
    NUMBER
    NUMBER OF SPARES
                                               Ω
                                               CIRCULAR
    CONFIGURATION
    DIMENSIONS FT
                                               100
                                               1000000
    CAPACTTY
                                               CARBON STEEL
    SHELL GENERIC MATERIAL TYPE
    SHELL SPECIFIC MATERIAL TYPE
                                              AISI 1110
    LINER GENERIC MATERIAL TYPE
                                              ORGANIC
    LINER SPECIFIC MATERIAL TYPE
                                               GLASS FLAKE-FILLED POLYESTER
    FEED STREAM SOURCE
                                               ABSORBER BLEED
                                               40.0%
    OUTLET STREAM CHARACTERISTICS
*** SLUDGE
    FULL LOAD SLUDGE QUANTITY - M.TONS/HR (DRY) 25.4
                                                             ( 28.0 TPH)
    MOISTURE CONTENT % TOTAL FREE WATER
                                                  60.0
    % CASO3 DRY
% CASO4 - DRY
                                                  18.0
                                                   5.0
    % CAOH2 - DRY
                                                   1.0
    % CACO3 - DRY
                                                   1.0
    % ASH - DRY
                                                  75.0
    % OTHER COMPOUNDS - DRY
                                                   1.0
** TREATMENT
    METHOD
                                               NONE
    DEVICE
                                               NR
    PROPRIETARY PROCESS
                                               NR
** DISPOSAL
    NATURE
                                               FTNAI
    TYPE
                                               POND
    LOCATION
                                               ON-SITE
    SITE TRANSPORTATION METHOD
                                               PIPELINE
    SITE TREATMENT
                                               NONE
    SITE DIMENSIONS
                                               70 ACRES/55 FT
    SITE CAPACITY - CU.M
                                                 4708550 ( 3850.0 ACRE-FT)
    SITE SERVICE LIFE - YRS
                                                10
** PROCESS CONTROL AND INSTRUMENTATION
    PROCESS STREAM
                                               SLURRY STREAM
    CHEMICAL PARAMETERS
                                               PH
    PHYSICAL VARIABLES
                                               % SOLIDS, FLOW, TEMPERATURE
    CONTROL LEVELS
                                               PH 6.2-7.2, 12% SOLIDS
    MONITOR TYPE
                                               PH- APS FLOW THROUGH; DENSITY- TEXAS NUCLEAR
    MONITOR LOCATION
                                               RECYCLE LOOP ON TANGENTIAL NOZZLE HEADER
    PROCESS CONTROL MANNER
                                               AUTOMATIC
    PROCESS CHEMISTRY MODE
                                               FEEDBACK
** WATER BALANCE
    WATER LOOP TYPE
                                               OPEN
    EVAPORATION WATER LOSS - LITER/S
                                                   6.3
                                                             ( 100 GPM)
    SOURCE OF MAKEUP WATER
                                               LAKE WATER
```

720

ARIZONA PUBLIC SERVICE: FOUR CORNERS 1 (CONT.)

FUNAPP SC CC UT PC AI	EMICALS AND CONSUM JNCTION AME RINCIPAL CONSTITUIN DURCE/SUPPLIER DNSUMPTION TILIZATION - % DINT OF ADDITION D SPARE CAPACITY BSORBER - % D SPARE COMPONENT BSORBER	ENT	ABSORBENT LIME CAO CAN AM, PAUL LI 20 TPD 83.0 SLAKER, ABSORBE			
PERIOD	MODULE AVAILABIL	ITY OPERABILITY RELIABIL	LITY UTILIZATION	% REMOVAL SO2 PART.	PER BOILER	FGD CAP.
	SYSTEM				720	
	SYSTEM				744	
12///	** PROBLEMS/SOLU	TIONS/COMMENTS			, , , ,	
	T NODELINO, GOLO	INITIAL OPERATIONS STA	ARTED IN NOVEMBER	1979.		
1/80	SYSTEM				744	
2/80	SYSTEM				696	
3/80	SYSTEM				744	
	** PROBLEMS/SOLU	TIONS/COMMENTS				
		THE UNIT IS PRESENTLY	IN THE SHAKEDOWN	√DEBUGGING F	PHASE OF OPER	ATION.
4/80	SYSTEM				720	
5/80	SYSTEM				744	
6/80	SYSTEM				720	
	** PROBLEMS/SOLU	TIONS/COMMENTS				
		ALTHOUGH THE FGD SYSTE REPORTED THAT IT IS UN				UTILITY
7/80	SYSTEM				744	
8/80	SYSTEM				744	
9/80	SYSTEM				720	
10/80	SYSTEM				744	
11/80	SYSTEM				720	
12/80	SYSTEM				744	
1/81	SYSTEM				744	
2/81	SYSTEM				672	
3/81	SYSTEM				744	

4/81 SYSTEM

ARIZONA PUBLIC SERVICE: FOUR CORNERS 1 (CONT.)

		AVAILABILITY					% REN	10VAL	PER		FGD	CAP.
5/81	SYSTEM								744			
6/81	SYSTEM								720			
7/81	SYSTEM								744			
8/81	SYSTEM								744			
9/81	SYSTEM								720			
10/81	SYSTEM								744			
11/81	SYSTEM								720			
12/81	SYSTEM								744			
1/82	SYSTEM								744			
2/82	SYSTEM								672			
3/82	SYSTEM								744			
4/82	SYSTEM								720			
5/82	SYSTEM								744			
6/82	SYSTEM								720			
7/82	SYSTEM								744			
8/82	SYSTEM								744			
9/82	SYSTEM								720			
10/82	SYSTEM								744			
11/82	SYSTEM								720			
12/82	SYSTEM								744			
1/83	SYSTEM								744			
2/83	SYSTEM								672			
3/83	SYSTEM								744			
	** PROB	LEMS/SOLUTION	15/COMMENTS									
		11	REORMATION WA	S UNAVAILABL	E FOR	THE PE	RIOD O	F JULY	1980	THROUGH	MARCH	1983.
4/83	SYSTEM								720			
5/83	SYSTEM								744			
6/83	SYSTEM								720			
	** PROB	LEMS/SOLUTION	IS/COMMENTS									
		I	FORMATION WA	S UNAVAILABL	E FOR	THE PER	RIOD O	F JULY	1980	THROUGH	JUNE	1983.
7/83	SYSTEM								744			
8/83	SYSTEM								744			

				PERFORMANCE	DATA					
PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY UT	ILIZATIO				BOILER HOURS	
9/83	SYSTEM							720		
	** PROE	BLEMS/SOLUTION	NS/COMMENTS							
		I	NFORMATION WA	AS UNAVAILABLE	FOR THE	THIRD Q	JARTER	OF 198	33.	
10/83	SYSTEM							744		
11/83	SYSTEM							720		
12/83	SYSTEM							744		
	** PROS	BLEMS/SOLUTIO	NS/COMMENTS							
		II	NFORMATION WA	AS UNAVAILABLE	FOR THE I	FOURTH (WARTER	7 OF 19	983.	
1/84	SYSTEM							744		
2/84	SYSTEM							696		
3/84	SYSTEM							744		
4/84	SYSTEM							720		
5/84	SYSTEM							744		
6/84	SYSTEM							720		
7/84	SYSTEM							744		
8/84	SYSTEM							744		
9/84	SYSTEM							720		

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS NOT AVAILABLE FOR THE FIRST THREE QUARTERS OF 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COMPANY NAME PLANT NAME UNIT NUMBER CITY STATE REGULATORY CLASSIFICATION PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW NET UNIT GENERATING CAPACITY W/FGD - MW NET UNIT GENERATING CAPACITY W/FGD - MW	ARIZONA PUBLIC SERVICE FOUR CORNERS 2 FRUITLAND NEW MEXICO C 21. ('.050 LB/MMBTU) 365. (.850 LB/MMBTU) 301. (.700 LB/MMBTU) 2085 195 170 175
EQUIVALENT SCRUBBED CAPACITY - MW	195
** UNIT DATA - BOILER AND STACK BOILER SUPPLIER BOILER TYPE BOILER SERVICE LOAD DESIGN BOILER FLUE GAS FLOW - CU.M/S BOILER FLUE GAS TEMPERATURE - C STACK HEIGHT M STACK SHELL STACK TOP DIAMETER - M	RILEY STOKER PULVERIZED COAL BASE 384.13 (814000 ACFM) 171.1 (340 F) 76. (250 FT) CONCRETE 5.3 (17.5 FT)
** FUEL DATA FUEL TYPE FUEL GRADE AVERAGE HEAT CONTENT - J/G RANGE HEAT CONTENT BTU/LB AVERAGE ASH CONTENT - % RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - % AVERAGE SULFUR CONTENT - % RANGE SULFUR CONTENT - % RANGE SULFUR CONTENT - % RANGE CHLORIDE CONTENT % RANGE CHLORIDE CONTENT %	COAL SUBBITUMINOUS 20004. (8600 BTU/LB) 8500-9100 22.00 19-25 10.80 8.5-13.4 .75 .5-1.3 .03 .0106
*** PARTICLE CONTROL	
AND PARTICLE CONTROL	
** MECHANICAL COLLECTOR NUMBER TYPE ** ESP NUMBER	0 NONE 0
TYPE	NONE
VVV FOR OVERFUL	
*** FGD SYSTEM	
** GENERAL DATA SALEABLE PRODUCT/THROWAWAY PRODUCT SO2 REMOVAL MODE PROCESS TYPE PROCESS ADDITIVES SYSTEM SUPPLIER A-E FIRM DEVELOPMENT LEVEL NEH/RETROFIT UNIT DESIGN PARTICLE REMOVAL EFFICIENCY UNIT DESIGN SO2 REMOVAL EFFICIENCY - % ENERGY CONSUMPTION - % CURPENT STATUS COMMERCIAL START-UP INITIAL START-UP CONTRACT AWARDED	THROWAWAY PRODUCT WET SCRUBBING LIME/ALKALINE FLYASH NONE GE ENVIRONMENTAL SERVICES IN-HOUSE FULL SCALE RETROFIT % 99.50 50.00 2.6 1 11/79 11/79 0/78

ARIZONA PUBLIC SERVICE: FOUR CORNERS 2 (CONT.)

```
** DESIGN AND OPERATING PARAMETERS
   DESIGN COAL SULFER CONTENT %
                                                  1.30
                                               19771.0
                                                              ( 8500 BTU/LB)
   DESIGN COAL HEAT CONTENT - J/G
   DESIGN COAL ASH CONTENT - %
                                                 25.00
   DESIGN MOISTURE CONTENT - %
                                                  13.40
   DESIGN CHLORIDE CONTENT - %
                                                   .06
                                                              ( 5600 SQ FT)
   SPACE REQUIREMENTS - SQ M
                                                 520.2
   OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                 200.0
** QUENCHER/PRESATURATOR
   CONSTRUCTION MATERIAL GENERIC TYPE
                                               NR
    CONSTRUCTION MATERIAL SPECIFIC TYPE
** ABSORBER
    NUMBER
                                                2
    NUMBER OF SPARES
                                                0
    GENERIC TYPE
                                               VENTURI TOWER
                                               VARIABLE-THROAT/TOP-ENTRY PLUMB BOB
    SPECIFIC TYPE
    TRADE NAME/COMMON TYPE
                                               N/A
    DIMENSIONS - FT
                                               25 DIA
    SHELL GENERIC MATERIAL
                                               CARBON STEEL
    SHELL SPECIFIC MATERIAL
                                               AISI 1110
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                               N/A
    LINER GENERIC MATERIAL
                                               OPGANTO
    LINER SPECIFIC MATERIAL
                                               GLASS FLAKE-FILLED POLYESTER
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                               FLAKELINE 103
    GAS CONTACTING DEVICE TYPE
                                               VENTURI THROAT [TANGENTIAL NOZZLES AT TOP & AT S
    NUMBER OF CONTACTING ZONES
                                                1
    LIQUID RECIRCULATION RATE - LITER/S
                                                630.
                                                              (10000 GPM)
                                                              ( 24.0 GAL/1000 ACF)
    L/G RATIO - L/CU.M
                                                   3.2
    GAS-SIDE PRESSURE DROP - KPA
                                                   2.5
                                                              (10.0 IN-H20)
                                                              ( 407000 ACFM)
    INLET GAS FLOW - CU. M/S
                                                 192.06
    INLET GAS TEMPERATURE - C
                                                 171.1
                                                              ( 340 F)
    SO2 REMOVAL EFFICIENCY - %
                                                  67.5
    PARTICLE REMOVAL EFFICENCY - %
                                                  99.5
** MIST ELIMINATOR
                                               PRIMARY COLLECTOR
    PRE-MIST ELIMINATOR/MIST ELIMINATOR
    NUMBER PER SYSTEM
                                                2
    NUMBER OF SPARES PER SYSTEM
                                                0
    NUMBER PER MODULE
                                                1
    GENERIC TYPE
                                               IMPINGEMENT
                                               BAFFLE
    SPECIFIC TYPE
    TRADE NAME/COMMON TYPE
                                               CLOSED VANE
                                               HORIZONTAL
    CONFIGURATION
    NUMBER OF STAGES
                                                   1
    NUMBER OF PASSES PER STAGE
                                                   ٨
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               ORGANIC
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               FIBER-REINFORCED POLYESTER
    WASH WATER SOURCE
                                               FRESH [FROM LAKE]
    WASH FREQUENCY
                                               ONCE PER SHIFT
** REHEATER
                                                0
    NUMBER
                                               NONE
    GENERIC TYPE
    SPECIFIC TYPE
                                               N/A
    TRADE NAME/COMMON TYPE
                                               N/A
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               NONE
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               N/A
** FANS
    NUMBER
                                                2
    NUMBER OF SPARES
    DESTGN
                                               CENTRIFUGAL
    SUPPLIER
                                               AMERICAN STANDARD
    FUNCTION
                                               UNTT
                                               INDUCED DRAFT
    APPLICATION
    SERVICE
                                               WET
    FLUE GAS FLOW RATE CU.M/S
                                                259.54
                                                              ( 550000 ACFM)
    FLUE GAS TEMPERATURE C
                                                  51.7
                                                              ( 125 F)
```

ARIZONA PUBLIC SERVICE: FOUR CORNERS 2 (CONT.)

CONSTRUCTION MATERIAL GENERIC TYPE	HIGH ALLOY
** DAMPERS NUMBER FUNCTION GENERIC TYPE SPECIFIC TYPE MANUFACTURER SERVICE CONDITIONS CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	2 CONTROL LOUVER PARALLEL BLADE MULTILOUVER AMERICAN STANDARD 120-130 F STAINLESS STEEL AUSTENITIC NONE N/A
** DAMPERS NUMBER FUNCTION GENERIC TYPE SPECIFIC TYPE MANUFACTURER SERVICE CONDITIONS CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	1 SHUT-OFF GUILLOTINE NR NR NR CARBON STEEL AISI 1110 NONE N/A
** DUCTWORK LOCATION CONFIGURATION DIMENSIONS SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	INLET CIRCULAR 14 DIA X 90 FT CARBON STEEL ASTM A-283 NONE N/A
** DUCTWORK LOCATION CONFIGURATION DIMENSIONS SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	OUTLET [ME TO STACK] RECTANGULAR 12 X 12 X 50 FT CARBON STEEL ASTM A-283 STAINLESS STEEL AUSTENITIC
** REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE DEVICE TYPE MANUFACTURER NUMBER NUMBER FULL LOAD DRY FEED CAPACITY - M.TONS/HR PRODUCT QUALITY - % SOLIDS	SLAKER NR NR JOY 1 0 13.6 (15 TPH) 30.0
** REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE DEVICE TYPE MANUFACTURER NUMBER NUMBER OF SPARES	WET BALL MILL NR NR KENNEDY VAN SAUN 1
** TANKS SERVICE BLEED STREAM RECYCLE MAKEUP WATER RETURN TRANSFER LIME SLURRY	NUMBER 1 2 1 1 4

ARIZONA PUBLIC SERVICE: FOUR CORNERS 2 (CONT.)

** PUMPS

```
NUMBER
   SERVICE
                                                  2
    RECYCLE
    RECYCLE [STANDBY]
                                                  4
    BLEED STREAM TANK
    THICKENER UNDERFLOW
                                                  4
    LIME SLURRY TRANSFER
                                                  2
    RETURN WATER
                                                  2
    SERVICE WATER
    ME WATER
                                                ***
** SOLIDS CONCENTRATING/DEWATERING
    DEVICE
                                               THICKENER
    NUMBER
                                                1
    NUMBER OF SPARES
                                               0
    CONFIGURATION
                                               CIRCULAR
    DIMENSIONS - FT
                                               100
    CAPACITY
                                               1000000
    SHELL GENERIC MATERIAL TYPE
                                               CARBON STEEL
    SHELL SPECIFIC MATERIAL TYPE
                                               AISI 1110
    LINER GENERIC MATERIAL TYPE
                                               ORGANIC
    LINER SPECIFIC MATERIAL TYPE
                                              GLASS FLAKE-FILLED POLYESTER
    FEED STREAM SOURCE
                                               ABSORBER BLEED
    OUTLET STREAM CHARACTERISTICS
                                               40.0%
*** SLUDGE
    FULL LOAD SLUDGE QUANTITY - M.TONS/HR (DRY) 25.4
                                                             ( 28.0 TPH)
    MOISTURE CONTENT - % TOTAL FREE WATER
                                                  60.0
    % CASO3 - DRY
                                                  18.0
    % CASO4 - DRY
                                                   5.0
    % CAOH2 - DRY
                                                   1.0
    % CACO3 - DRY
                                                   1.0
    % ASH - DRY
                                                   75.0
    % OTHER COMPOUNDS - DRY
                                                   1.0
 ** TREATMENT
    METHOD
                                               NONE
                                                NR
    DEVICE
    PROPRIETARY PROCESS
                                                NR
 ** DISFOSAL
                                                FTNAI
    NATURE
    TYPE
                                                POND
                                                ON-SITE
    LOCATION
    SITE TRANSPORTATION METHOD
                                                PIPELINE
    SITE TREATMENT
                                               NONE
    SITE DIMENSIONS
                                                70 ACRES/55 FT
                                                  4708550 ( 3850.0 ACRE-FT)
    SITE CAPACITY - CU.M
    SITE SERVICE LIFE - YRS
 ** PROCESS CONTROL AND INSTRUMENTATION
                                                SLURRY STREAM
    PROCESS STREAM
    CHEMICAL PARAMETERS
                                                PH
                                                % SOLIDS, FLOW, TEMPERATURE
    PHYSICAL VARIABLES
    CONTROL LEVELS
                                               PH 6.2-7.2, 12% SOLIDS
    MONITOR TYPE
                                               PH- APS FLOW THROUGH; DENSITY- TEXAS NUCLEAR
                                               RECYCLE LOOP ON TANGENTIAL NOZZLE HEADER
    MONITOR LOCATION
    PROCESS CONTROL MANNER
                                               AUTOMATIC
    PROCESS CHEMISTRY MODE
                                               FEEDBACK
 ** WATER BALANCE
    WATER LOOP TYPE
                                                              ( 100 GPM)
    EVAPORATION WATER LOSS - LITER/S
                                                  6.3
    SOURCE OF MAKEUP WATER
                                                LAKE WATER
```

ARIZONA PUBLIC SERVICE: FOUR CORNERS 2 (CONT.)

** CHEMICALS AND CONSUMPTION

FUNCTION ABSORBENT NAME LIME PRINCIPAL CONSTITUENT CAO

SOURCE/SUPPLIER CAN AM, PAUL LIME CO.

CONSUMPTION 20 TPD UTILIZATION % 83.0

POINT OF ADDITION SLAKER, ABSORBER BOTTOM

** FGD SPARE CAPACITY INDICES

ABSORBER - % .0

** FGD SPARE COMPONENT INDICES

12/79 SYSTEM

ABSORBER .0

PERFORMANCE DATA	
PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZ	TION / REMOVAL PER BOILER FGD CAP. SD2 PART. HOURS HOURS HOURS FACTOR
	SUZ PART. HOURS HOURS FACTOR
11/79 SYSTEM	720

** PROBLEMS/SOLUTIONS/COMMENTS

INITIAL OPERATIONS STARTED IN NOVEMBER 1979.

1/80	SYSTEM	744
2/80	SYSTEM	696
3/80	SYSTEM	744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT IS PRESENTLY IN THE SHAKEDOWN/DEBUGGING PHASE OF OPERATION.

744

4/80	SYSTEM	720
5/80	SYSTEM	744
6/80	SYSTEM	720

** PROBLEMS/SOLUTIONS/COMMENTS

ALTHOUGH THE FGD SYSTEM PERFORMANCE DATA ARE BEING LOGGED, THE UTILITY REPORTED THAT IT IS UNAVAILABLE FOR RELEASE AT THIS TIME.

7/80	SYSTEM	
8/80	SYSTEM	
9/80	SYSTEM	
10/80	SYSTEM	
11/80	SYSTEM	
12/80	SYSTEM	
1/81	SYSTEM	
2/81	SYSTEM	
3/81	SYSTEM	
4/81	SYSTEM	

PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATIO	N % REI 502	MOVAL PART.	PER HOURS	BOILER HOURS	FGD HOURS	CAP. FACTOR
	SYSTEM							744			
	SYSTEM							720			
	SYSTEM							744			
								744			
	SYSTEM							720			
	SYSTEM							744			
	SYSTEM							720			
	SYSTEM							744			
	SYSTEM							744			
	SYSTEM							672			
	SYSTEM							744			
	SYSTEM							720 744			
	SYSTEM							720			
	SYSTEM							744			
	SYSTEM							744			
	SYSTEM							720			
	SYSTEM							744			
	SYSTEM							720			
	SYSTEM							744			
	SYSTEM							744			
	SYSTEM							672			
	SYSTEM							744			
		BLEMS/SOLUTIO	NS/COMMENTS								
			NFORMATION W	AS UNAVAILAB	LE FOR THE	PERIOD	OF JUL	Y 1980	THROUG	H MARCH	i 1983.
4/83	SYSTEM							720			
5/83	SYSTEM							744			
6/83	SYSTEM							720			
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
		I	NFORMATION W	AS UNAVAILAB	LE FOR THE	PERIOD	OF JUL	Y 1980	THROUG	Н ЈИМЕ	1983.
7/83	SYSTEM							744			
8/83	SYSTEM							744			

ARIZONA PUBLIC SERVICE: FOUR CORNERS 2 (CONT.)

	PERFORMANCE DATA		
PERIOD	MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION	% REMOVAL PER BOILER F	
9/83	SYSTEM	720	
	** PROBLEMS/SOLUTIONS/COMMENTS		
	INFORMATION WAS UNAVAILABLE FOR THE TH	IRD QUARTER OF 1983.	
10/83	SYSTEM	744	
11/83	SYSTEM	720	
12/83	SYSTEM	744	
	** PROBLEMS/SOLUTIONS/COMMENTS		
	INFORMATION WAS UNAVAILABLE FOR THE FO	JRTH QUARTER OF 1983.	
1/84	SYSTEM	744	
2/84	SYSTEM	696	
3/84	SYSTEM	744	
4/84	SYSTEM	720	
5/84	SYSTEM	744	
6/84	SYSTEM	720	
7/84	SYSTEM	744	

** PROBLEMS/SOLUTIONS/COMMENTS

8/84 SYSTEM

9/84 SYSTEM

INFORMATION WAS NOT AVAILABLE FOR THE FIRST THREE QUARTERS OF 1984.

744

720

```
ARIZONA PUBLIC SERVICE
COMPANY NAME
PLANT NAME
                                                FOUR CORNERS
UNIT NUMBER
                                               FRUITLAND
CITY
STATE
                                               NEW MEXICO
REGULATORY CLASSIFICATION
                                               С
                                                             ( .050 LB/MMBTU)
( .850 LB/MMBTU)
( .700 LB/MMBTU)
PARTICULATE EMISSION LIMITATION - NG/J
                                                  21.
                                                365.
502 EMISSION LIMITATION - NG/J
                                                301.
NOX EMISSION LIMITATION - NG/J
                                               2085
NET PLANT GENERATING CAPACITY - MW
                                               225
196
GROSS UNIT GENERATING CAPACITY - MW
NET UNIT GENERATING CAPACITY W/FGD - MW
NET UNIT GENERATING CAPACITY WO/FGD - MW
                                                495
EQUIVALENT SCRUBBED CAPACITY - MW
                                                 225
 ** UNIT DATA - BOILER AND STACK
    BOILER SUPPLIER
                                               RILEY STOKER
    BOILER TYPE
                                               PULVERIZED COAL
    BOILER SERVICE LOAD
                                               BASE
    DESIGN BOILER FLUE GAS FLOW - CU.M/S
                                              486.06
171.1
                                                              (1030000 ACFM)
     BOILER FLUE GAS TEMPERATURE - C
                                                             ( 340 F)
    STACK HEIGHT - M
                                                              ( 250 FT)
                                                 76.
     STACK SHELL
                                               CONCRETE
     STACK TOP DIAMETER - M
                                                *****
                                                              (**** FT)
 ** FUEL DATA
    FUEL TYPE
                                                COAL
     FUEL GRADE
                                                SUBBITUMINOUS
                                                20004.
     AVERAGE HEAT CONTENT - J/G
                                                             ( 8600 BTU/LB)
     RANGE HEAT CONTENT - BTU/LB
                                                               8500-9100
     AVERAGE ASH CONTENT - %
                                                  22.00
     RANGE ASH CONTENT - %
                                                19-25
     AVERAGE MOISTURE CONTENT - %
                                                 10.80
     RANGE MOISTURE CONTENT - %
                                                8.5-13.4
     AVERAGE SULFUR CONTENT %
                                                   . 75
     RANGE SULFUR CONTENT - %
     AVERAGE CHLORIDE CONTENT - %
                                                   . 03
     RANGE CHLORIDE CONTENT - X
                                                .01-.06
*** PARTICLE CONTROL
 ** MECHANICAL COLLECTOR
     NUMBER
                                                 0
     TYPE
                                                NONE
 ** ESP
     NUMBER
                                                 0
     TYPE
                                                HONE
*** FGD SYSTEM
 ** GENERAL DATA
                                               THROWAWAY PRODUCT
     SALEABLE PRODUCT/THROWAWAY PRODUCT
                                                WET SCRUBBING
     SO2 REMOVAL MODE
     PROCESS TYPE
                                                LIME/ALKALINE FLYASH
     PROCESS ADDITIVES
                                                NONE
     SYSTEM SUPPLIER
                                                GE ENVIRONMENTAL SERVICES
     A-E FIRM
                                                IN-HOUSE
                                                FULL SCALE
     DEVELOPMENT LEVEL
     NEW/RETROFIT
                                                RETROFIT
     UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.50
     UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                  50.00
     CURRENT STATUS
                                                1
                                                11/79
     COMMERCIAL START-UP
     INITIAL START-UP
                                                11/79
                                                 0/78
     CONTRACT AWARDED
```

ARIZONA PUBLIC SERVICE: FOUR CORNERS 3 (CONT.)

```
** DESIGN AND OPERATING PARAMETERS
   DESIGN COAL SULFER CONTENT - %
                                                 1.30
                                                            ( 8500 BTU/LB)
   DESIGN COAL HEAT CONTENT - J/G
                                              19771.0
   DESIGN COAL ASH CONTENT - %
                                                25.00
   DESIGN MOISTURE CONTENT - %
                                                 13.40
                                                   .06
   DESIGN CHLORIDE CONTENT - %
                                                            ( 5600 SQ FT)
                                                520.2
   SPACE REQUIREMENTS SQ M
   OPER. & MAINT, REQUIREMENT - MANHR/DAY
                                               200.0
** QUENCHER/PRESATURATOR
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              ND
   CONSTRUCTION MATERIAL SPECIFIC TYPE
** ABSORBER
   NUMBER
                                               2
   NUMBER OF SPARES
                                              VENTURI TOWER
   GENERIC TYPE
   SPECIFIC TYPE
                                              VARIABLE-THROAT/TOP-ENTRY PLUMB BOB
    TRADE NAME/COMMON TYPE
                                              N/A
   DIMENSIONS - FT
                                              25 DIA
                                              CARBON STEEL
    SHELL GENERIC MATERIAL
    SHELL SPECIFIC MATERIAL
                                              AISI 1110
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                              N/A
    LINER GENERIC MATERIAL
                                              ORGANIC
    LINER SPECIFIC MATERIAL
                                              GLASS FLAKE-FILLED POLYESTER
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                              FLAKELINE 103
    GAS CONTACTING DEVICE TYPE
                                              VENTURI THROAT [TANGENTIAL NOZZLES AT TOP & AT S
   NUMBER OF CONTACTING ZONES
    L/G RATIO - L/CU.M
                                                  3.2
                                                            ( 24.0 GAL/1000 ACF)
    GAS-SIDE PRESSURE DROP - KPA
                                                  2.5
                                                            (10.0 IN-H20)
                                              171.1
    INLET GAS TEMPERATURE - C
                                                            ( 340 F)
    SO2 REMOVAL EFFICIENCY - %
                                                67.5
    PARTICLE REMOVAL EFFICENCY - %
                                                 99.5
** MIST ELIMINATOR
    PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                              PRIMARY COLLECTOR
   NUMBER PER SYSTEM
                                               2
    NUMBER OF SPARES PER SYSTEM
                                               0
    NUMBER PER MODULE
                                               1
    GENERIC TYPE
                                              IMPINGEMENT
    SPECIFIC TYPE
                                              BAFFLE
    TRADE NAME/COMMON TYPE
                                              CLOSED VANE
    CONFIGURATION
                                              HORIZONTAL
   NUMBER OF STAGES
                                                  1
   NUMBER OF PASSES PER STAGE
                                                  6
    CONSTRUCTION MATERIAL GENERIC TYPE
                                             ORGANIC
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                             FIBER-REINFORCED POLYESTER
   WASH WATER SOURCE
                                              FRESH [FROM LAKE]
   WASH FREQUENCY
                                              ONCE PER SHIFT
** REHEATER
   NUMBER
                                               a
    GENERIC TYPE
                                              NONE
    SPECIFIC TYPE
                                              N/A
    TRADE NAME/COMMON TYPE
                                              N/A
    CONSTRUCTION MATERIAL GENERIC TYPE
                                              NONE
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              N/A
** FANS
   NUMBER
                                               2
   NUMBER OF SPARES
                                               ٥
   DESIGN
                                              CENTRIFUGAL
    SUPPLIER
                                              AMERICAN STANDARD
    FUNCTION
                                              NR
   APPLICATION
                                              INDUCED DRAFT
   SERVICE
                                              WET
   FLUE GAS TEMPERATURE - C
                                                51.7
                                                             ( 125 F)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                             HIGH ALLOY
```

ARIZONA PUBLIC SERVICE: FOUR CORNERS 3 (CONT.)

** DAMPERS NUMBER FUNCTION GENERIC TYPE SPECIFIC TYPE MANUFACTURER SERVICE CONDITIONS CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	2 CONTROL LOUVER PARALLEL BLADE MULTILOUVER AMERICAN STANDARD 120-130 F STAINLESS STEEL AUSTENITIC NONE N/A
** DAMPERS NUMBER FUNCTION GENERIC TYPE SPECIFIC TYPE MANUFACTURER SERVICE CONDITIONS CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	1 SHUT-OFF GUILLOTINE NR NR NR CARBON STEEL AISI 1110 NONE N/A
** DUCTWORK LOCATION CONFIGURATION DIMENSIONS SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	INLET CIRCULAR NR CARBON STEEL ASTM A-283 NONE N/A
** DUCTWORK LOCATION CONFIGURATION DIMENSIONS SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	OUTLET [ME TO STACK] RECTANGULAR NR CARBON STEEL ASTM A-283 STAINLESS STEEL AUSTENITIC
** REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE DEVICE TYPE MANUFACTURER NUMBER NUMBER FULL LOAD DRY FEED CAPACITY - M.TONS/HR PRODUCT QUALITY // SOLIDS	SLAKER NR NR JOY 1 0 13.6 (15 TPH) 30.0
** REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE DEVICE TYPE MANUFACTURER NUMBER NUMBER OF SPARES	WET BALL MILL NR NR KENNEDY VAN SAUN 1 0
** TANKS SERVICE BLEED STREAM RECYCLE MAKEUP WATER RETURN TRANSFER LIME SLURRY	NUMBER 1 2 1 1 4

ARIZONA PUBLIC SERVICE: FOUR CORNERS 3 (CONT.)

```
** PUMPS
                                               NUMBER
    SERVICE
                                               -----
    RECYCLE
    RECYCLE [STANDBY]
    BLEED STREAM TANK
                                                4
    THICKENER UNDERFLOW
    LIME SLURRY TRANSFER
    RETURN WATER
    SERVICE WATER
                                               ****
                                               ****
    ME WATER
** SOLIDS CONCENTRATING/DEWATERING
                                               THICKENER
    DEVICE
    NUMBER
                                               1
    NUMBER OF SPARES
                                               0
                                              CIRCULAR
    CONFIGURATION
                                              100
    DIMENSIONS - FT
                                              1000000
    CAPACITY
    SHELL GENERIC MATERIAL TYPE
                                              CARBON STEEL
                                              AISI 1110
    SHELL SPECIFIC MATERIAL TYPE
                                             ORGANIC
GLASS FLAKE-FILLED POLYESTER
ABSORBER BLEED
    LINER GENERIC MATERIAL TYPE
    LINER SPECIFIC MATERIAL TYPE
    FEED STREAM SOURCE
    OUTLET STREAM CHARACTERISTICS
                                              40.0%
*** SLUDGE
                                                            ( 28.0 TPH)
    FULL LOAD SLUDGE QUANTITY - M.TONS/HR (DRY) 25.4
    MOISTURE CONTENT % TOTAL FREE WATER
                                                 60.0
    % CAS03 - DRY
                                                  18.0
    % CASO4 - DRY
                                                  5.0
    % CAOH2 - DRY
                                                   1.0
    % CACO3 - DRY
                                                  1.0
    % ASH - DRY
                                                  75.0
    % OTHER COMPOUNDS - DRY
 ** TREATMENT
                                              NONE
    METHOD
    DEVICE
    PROPRIETARY PROCESS
                                               NP
 ** DISPOSAL
    NATURE
                                               FINAL
    TYPE
                                               DUND
    LOCATION
                                               ON-SITE
    SITE TRANSPORTATION METHOD
                                              PIPELINE
     SITE TREATMENT
                                              NONE
     SITE DIMENSIONS
                                              70 ACRES/55 FT
     SITE CAPACITY - CU.M
                                                 4708550 ( 3850.0 ACRE-FT)
     SITE SERVICE LIFE - YRS
                                               10
 ** PROCESS CONTROL AND INSTRUMENTATION
    PROCESS STREAM
                                               SLURRY STREAM
     CHEMICAL PARAMETERS
                                               PH
    PHYSICAL VARIABLES
                                               % SOLIDS, FLOW, TEMPERATURE
    CONTROL LEVELS
                                               PH 6.2-7.2, 12% SOLIDS
    MONITOR TYPE
                                               PH- APS FLOW THROUGH; DENSITY- TEXAS NUCLEAR
    MONITOR LOCATION
                                             RECYCLE LOOP ON TANGENTIAL NOZZLE HEADER
    PROCESS CONTROL MANNER
                                               AUTOMATIC
    PROCESS CHEMISTRY MODE
                                              FEEDBACK
 ** WATER BALANCE
    WATER LOOP TYPE
    EVAPORATION WATER LOSS - LITER/S
                                                6.3 ( 100 GPM)
    SOURCE OF MAKEUP WATER
                                              LAKE WATER
```

720

ARIZONA PUBLIC SERVICE: FOUR CORNERS 3 (CONT.)

** CHEMICALS AND CONSUMPTION

4/81 SYSTEM

FUNCTION ABSORBENT NAME LIME PRINCIPAL CONSTITUENT CAO SOURCE/SUPPLIER CAN AM, PAUL LIME CO. CONSUMPTION 20 TPD UTILIZATION - % 83.0 POINT OF ADDITION SLAKER, ABSORBER BOTTOM ** FGD SPARE CAPACITY INDICES ABSORBER - % .0 ** FGD SPARE COMPONENT INDICES ABSORBER .0 PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.
SO2 PART. HOURS HOURS FACTOR 11/79 SYSTEM 720 12/79 SYSTEM 744 ** PROBLEMS/SOLUTIONS/COMMENTS INITIAL OPERATIONS STARTED IN NOVEMBER 1979. 1/80 SYSTEM 744 2/80 SYSTEM 696 3/80 SYSTEM 744 ** PROBLEMS/SOLUTIONS/COMMENTS THE UNIT IS PRESENTLY IN THE SHAKEDOWN/DEBUGGING PHASE OF OPERATION. 4/80 SYSTEM 720 5/80 SYSTEM 744 6/80 SYSTEM 720 ** PROBLEMS/SOLUTIONS/COMMENTS ALTHOUGH THE FGD SYSTEM PERFORMANCE DATA ARE BEING LOGGED, THE UTILITY REPORTED THAT IT IS UNAVAILABLE FOR RELEASE AT THIS TIME. 7/80 SYSTEM 744 8/80 SYSTEM 744 9/80 SYSTEM 720 10/80 SYSTEM 744 11/80 SYSTEM 720 12/80 SYSTEM 744 1/81 SYSTEM 744 2/81 SYSTEM 672 3/81 SYSTEM 744

PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZ	ZATIO	N % RE1 SO2	10VAL PART.	PER HOURS	BOILER HOURS	FGD HOURS	CAP.
5/81	SYSTEM								744			
6/81	SYSTEM								720			
7/81	SYSTEM								744			
8/81	SYSTEM								744			
9/81	SYSTEM								720			
10/81	SYSTEM								744			
11/81	SYSTEM								720			
12/81	SYSTEM								744			
1/82	SYSTEM								744			
2/82	SYSTEM								672			
3/82	SYSTEM								744			
4/82	SYSTEM								720			
5/82	SYSTEM								744			
6/82	SYSTEM								720			
7/82	SYSTEM						•		744			
8/82	SYSTEM								744			
9/82	SYSTEM								720			
10/82	SYSTEM								744			
11/82	SYSTEM								720			
12/82	SYSTEM								744			
1/83	SYSTEM								744			
2/83	SYSTEM								672			
3/83	SYSTEM								744			
	** PROB	LEMS/SOLUTION	NS/COMMENTS									
		I	NFORMATION WA	S UNAVAILABL	E FOR	THE I	PERIOD O	F JULY	1980	THROUGH	MARCH	1983.
4/83	SYSTEM								720			
5/83	SYSTEM								744			
6/83	SYSTEM								720			
	** PROB	LEMS/SOLUTION	NS/COMMENTS									
		It	NFORMATION WA	S UNAVAILABL	E FOR	THE I	PERIOD O	F JULY	1980	THROUGH	JUNE	1983.
7/83	SYSTEM								744			
8/83	SYSTEM								744			

				PERFORMANO	E DATA					
PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY U	JTILIZATI				BOILER HOURS	
9/83	SYSTEM							720		
	** PROE	LEMS/SOLUTIO	NS/COMMENTS							
		I	NFORMATION W	AS UNAVAILABLE	FOR THE	THIRD Q	JARTER	OF 198	33.	
10/83	SYSTEM							744		
11/83	SYSTEM							720		
12/83	SYSTEM							744		
	** PROE	BLEMS/SOLUTIO	NS/COMMENTS							
		I	NFORMATION W	AS UNAVAILABLE	FOR THE	FOURTH	QUARTE	R OF 19	983.	
1/84	SYSTEM							744		
2/84	SYSTEM							696		
3/84	SYSTEM							744		
4/84	SYSTEM							720		
5/84	SYSTEM							744		
6/84	SYSTEM							720		
7/84	SYSTEM			.9				744		
8/84	SYSTEM							744		
9/84	SYSTEM							720		

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS NOT AVAILABLE FOR THE FIRST THREE QUARTERS OF 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

ASSOCIATED ELECTRIC COMPANY NAME THOMAS HILL PLANT NAME UNIT NUMBER MORERLY CITY MISSOURI STATE WAXXXX

GRUSS UNIT GENERATING CAPACITY - MW 1150

NET UNIT GENERATING CAPACITY W/FGD - MW 667

NET UNIT GENERATING CAPACITY WO/FGD - MW 495

EQUIVALENT SCRUBBED CAPACITY - MW 170 ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER BABCOCK & WILCOX (***** ACFM) ** FUEL DATA FUEL TYPE COAL ***** FUEL GRADE AVERAGE HEAT CONTENT J/G RANGE HEAT CONTENT - BTU/LB 24423. (10500 BTU/LB) 11.20 ***** 9600-9800 AVERAGE ASH CONTENT - % RANGE ASH CONTENT - % AVERAGE SULFUR CONTENT - %

AVERAGE SULFUR CONTENT - %

RANGE SULFUR CONTENT - %

RANGE SULFUR CONTENT - % 14.00 ***** 4.80 3.8-4.5 ***** RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - % ***** *** PARTICLE CONTROL ** ESP NUMBER NUMBER OF SPARES 0 COLD SIDE PEABODY INTERNATIONAL TYPE SUPPLIER. INLET FLUE GAS CAPACITY - CU.M/S
INLET FLUE GAS TEMPERATURE - C 1349.6 (2860000 ACFM) 148.9 (300 F) 99.7 PARTICLE REMOVAL EFFICENCY - % ** PARTICLE SCRUBBER NUMBER 0 GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL N/A LINER GENERIC MATERIAL N/A LINER SPECIFIC MATERIAL N/A GAS CONTACTING DEVICE TYPE N/A *** FGD SYSTEM ** GENERAL DATA SALEABLE PRODUCT/THROWAWAY PRODUCT THROWAWAY PRODUCT SO2 REMOVAL MODE WET SCRUBBING PROCESS TYPE LIMESTONE PROCESS ADDITIVES MAG SYSTEM SUPPLIER M.W. KELLOGG

ASSOCIATED ELECTRIC: THOMAS HILL 3 (CONT.)

```
BURNS & MCDONNELL
   A-E FIRM
   DEVELOPMENT LEVEL
                                               FULL SCALE
   NEW/RETROFIT
                                               NEM
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.00
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                  91.50
   CURRENT STATUS
                                                1
   COMMERCIAL START-UP
                                               12/82
                                               10/82
   INITIAL START-UP
   CONTRACT AWARDED
                                                2/78
** DESIGN AND OPERATING PARAMETERS
   SPACE REQUIREMENTS - SQ M
                                               1858.0
                                                             ( 20000 SQ FT)
** QUENCHER/PRESATURATOR
   CONSTRUCTION MATERIAL GENERIC TYPE
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               NR
** ABSORBER
   NUMBER
                                                4
   NUMBER OF SPARES
                                                1
   GENERIC TYPE
                                               SPRAY TOWER
                                               OPEN CROSSCURRENT SPRAY
   SPECIFIC TYPE
   TRADE NAME/COMMON TYPE
                                               HORIZONTAL SPRAY CHAMBER
    SUPPLIER
                                               PULLMAN KELLOGG
                                               26.0 X 18.0 X 80.0
   DIMENSIONS - FT
    SHELL GENERIC MATERIAL
                                               CARBON STEEL
    SHELL SPECIFIC MATERIAL
                                               AISI 1110
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                               N/A
    LINER GENERIC MATERIAL
                                               INORGANIC
    LINER SPECIFIC MATERIAL
                                               PREFIRED BRICK/SHAPES
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                               ACID-RESISTANT BRICK [LOW H20 ABSORPTION]
    GAS CONTACTING DEVICE TYPE
                                               NONE
    NUMBER OF CONTACTING ZONES
                                                4
    LIQUID RECIRCULATION RATE - LITER/S
                                                              (42000 GPM)
                                                2646.
    L/G RATIO L/CU.M
                                                   2.3
                                                              ( 17.4 GAL/1000 ACF)
    GAS-SIDE PRESSURE DROP - KPA
                                                   .4
                                                              ( 1.5 IN-H20)
    SUPERFICAL GAS VELOCITY - M/SEC
                                                   6.7
                                                              ( 22.0 FT/S)
    INLET GAS FLOW - CU. M/S
                                                1142.00
                                                              (2420000 ACFM)
    INLET GAS TEMPERATURE - C
                                                 137.8
                                                              ( 280 F)
    SO2 REMOVAL EFFICIENCY - %
                                                  92.0
** MIST ELIMINATOR
                                               PRIMARY COLLECTOR
    PRE-MIST ELIMINATOR/MIST ELIMINATOR
   NUMBER PER SYSTEM
                                               IMPINGEMENT
   GENERIC TYPE
    SPECIFIC TYPE
                                               BAFFLE
    TRADE NAME/COMMON TYPE
                                               CLOSED VANE
   CONFIGURATION
                                               VERTICAL
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               NR
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               NΒ
    WASH FREQUENCY
                                               INTERMITTENT
** REHEATER
    GENERIC TYPE
                                               BYPASS
    SPECIFIC TYPE
                                               COLD SIDE
    TRADE NAME/COMMON TYPE
                                               N/A
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               NR
                                               NB
    CONSTRUCTION MATERIAL SPECIFIC TYPE
** FANS
   NUMBER
                                                2
   NUMBER OF SPARES
                                                ۵
                                               AXIAL
    DESIGN
    SUPPLIER
                                               TLT-BABCOCK
    FUNCTION
                                               UNITT
    APPLICATION
                                               FORCED DRAFT
    SERVICE
                                               DRY
    FLUE GAS FLOW RATE - CU.M/S
                                               1349.63
                                                              (2860000 ACFM)
    FLUE GAS TEMPERATURE - C
                                                 148.9
                                                              ( 300 F)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              CARBON STEEL
```

ASSOCIATED ELECTRIC: THOMAS HILL 3 (CONT.)

```
** FANS
    NUMBER
                                                 2
    NUMBER OF SPARES
                                                 0
                                                AXIAL
    DESIGN
                                                WESTINGHOUSE
    SUPPLIER
    FUNCTION
                                                UNIT
                                                FORCED DRAFT
    APPLICATION
    SERVICE
                                                DRY
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                CARBON STEEL
** DAMPERS
                                                NΒ
    FUNCTION
    GENERIC TYPE
                                                NR
    SPECIFIC TYPE
                                                ND
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                NR
                                                ΝR
    CONSTRUCTION MATERIAL SPECIFIC TYPE
    LINER GENERIC MATERIAL TYPE
                                                ΝŔ
    LINER SPECIFIC MATERIAL TYPE
                                                NR
** DUCTWORK
     SHELL GENERIC MATERIAL TYPE
                                                NR
                                                NR
     SHELL SPECIFIC MATERIAL TYPE
                                                NR
     LINER GENERIC MATERIAL TYPE
                                                NR
     LINER SPECIFIC MATERIAL TYPE
** REAGENT PREPARATION EQUIPMENT
                                                WET BALL MILL
    FUNCTION
    DEVICE
                                                COMPARTMENTED
    DEVICE TYPE
                                                NR
    MANUFACTURER
                                                KENNEDY VAN SAUN
    NUMBER
                                                 2
    NUMBER OF SPARES
                                                 0
    FULL LOAD DRY FEED CAPACITY - M.TONS/HR
                                                               ( 82 TPH)
                                                   74.4
** REAGENT PREPARATION EQUIPMENT
    FUNCTION
                                                SLAKER
    DEVICE
                                                NR
    DEVICE TYPE
                                                NR
    MANUFACTURER
                                                ΝŔ
** TANKS
    SERVICE
                                                NUMBER
                                                 -----
    LIMESTONE-SLURRY STORAGE
                                                   2
    MIST ELIMINATOR WASH
    FLOCCULANT
                                                 ***
    THICKENER OVERFLOW
                                                 ***
    ABSORBER RECYCLE
                                                 ****
    FORCED OXIDATION
                                                   2
    MILL-PRODUCT
** PUMPS
    SERVICE
                                                NUMBER
    ABSORBER RECIRCULATION
                                                  16
    WASH WATER
                                                 ****
    FLOCCULANT FEED
                                                 ****
    THICKENER UNDERFLOW
                                                 ****
    THICKENER OVERFLOW
                                                 ****
    LIMESTONE SLURRY TRANSFER
                                                   4
    MILL-PRODUCT
** SOLIDS CONCENTRATING/DEWATERING
    DEVICE
                                                 CENTRIFUGE
    NUMBER
                                                 7
** SOLIDS CONCENTRATING/DEWATERING
    DEVICE
                                                 THICKENER
    NUMBER
                                                 1
    DIMENSIONS FT
```

180.0 DIA

ASSOCIATED ELECTRIC: THOMAS HILL 3 (CONT.)

OUTLET STREAM CHARACTERISTICS 30% SOLIDS

*** SLUDGE

** TREATMENT

METHOD FORCED OXIDATION

DEVICE N/A
PROPRIETARY PROCESS N/A

** DISPOSAL

NATURE FINAL
TYPE LANDFILL
SITE TRANSPORTATION METHOD TRUCK
SITE TREATMENT NR

** PROCESS CONTROL AND INSTRUMENTATION

MONITOR TYPE KVB

** WATER BALANCE

WATER LOOP TYPE CLOSED

MAKEUP WATER ADDITION - LITERS/S 48.6 (772 GPM)

** CHEMICALS AND CONSUMPTION

FUNCTION ABSORBENT
NAME DOLOMITIC LIME
PRINCIPAL CONSTITUENT 60% CAO, 40% MGO
POINT OF ADDITION SLAKER

** FGD SPARE CAPACITY INDICES

ABSORBER - % 33.3

** FGD SPARE COMPONENT INDICES
ABSORBER 1.0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART, HOURS HOURS FACTOR

10/82 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT INITIAL START-UP OF THE FGD SYSTEM OCCURRED DURING OCTOBER, 1982.

DURING UCTUBER; 1902

11/82 SYSTEM 720

12/82 SYSTEM 744

1/83 SYSTEM 744

2/83 SYSTEM 672

3/83 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED PROBLEMS WITH A CENTRIFUGE IN THE SLUDGE DEWATERING PROCESS SECTION. THE INABILITY TO REDUCE THE SLUDGE SOLIDS CONTENT HAS

FORCED THE UTILITY TO OPERATE BELOW THE FULL LOAD DEMAND.

4/83 SYSTEM 720

5/83 SYSTEM 744

6/83 SYSTEM 720

ASSOCIATED ELECTRIC: THOMAS HILL 3 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

502 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE PERIOD OF APRIL THROUGH JUNE 1983.

7/83	3A1 3A2 3B1 3B2 SYSTEM	35.6 63.8 13.8 80.8 64.7	35.2 61.5 14.9 79.9 63.8	63.8	32.5 56.9 13.8 73.9 59.0	744	688	439	80.6
8/83	3A1 3A2 3B1 3B2 SYSTEM	36.7 51.3 59.3 50.0 65.7	36.8 51.4 59.4 50.1 65.9	65.9	36.7 51.3 59.3 50.0 65.7	744	742	489	93.5
9/83	3A1 3A2 3B1 3B2 SYSTEM	23.9 60.1 40.0 72.6 65.5	24.0 60.4 39.5 68.9 64.2	64.2	23.9 60.1 39.3 68.5 63.9	720	717	460	91.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY ENCOUNTERED MAJOR PROBLEMS IN ATTEMPTING TO OPERATE THE DE-WATERING PLANT AT REQUIRED CAPACITY FOR FULL FLUE GAS SCRUBBING. THESE PROBLEMS CENTERED AROUND THE CENTRIFUGE AND OXIDATION SYSTEM.

THE UTILITY EXPERIENCED CENTRIFUGE FAILURE WHILE DEWATERING UNDERFLOW TO THE REQUIRED SOLIDS CONCENTRATION. IN ATTEMPTS TO DUPLICATE CONDITIONS PRESENTED AT A TEST CENTRIFUGE, IT WAS DISCOVERED THAT OXIDIZED SLUDGE BELOW THE DESIGN SOLIDS CONCENTRATION TRIPS THE MACHINE ON TORQUE AND UNOXIDIZED SLUDGE BELOW THE DESIGN SOLIDS CONCENTRATION TRIPS THE MACHINE ON VIBRATION. THE UTILITY IS CONTINUING TO ADDRESS THE PROBLEM.

THE OXIDATION SYSTEM IS NOT UP TO REQUIRED CAPACITY. DURING THIS PERIOD WORK ON 2 OF 3 COMPRESSORS HAS BROUGHT UP THEIR CAPACITY, BUT PLUGGING OF THE SPARGER RINGS AND BUILD UP OF SOLIDS IN THE OXIDATION TANK CONTINUE TO ADVERSELY EFFECT THE OXIDATION CAPABILITIES. DESIGN FAILURE OF THE MIXING PADDLES HAS ALSO OCCURRED AND A TEMPORARY FIX WAS MADE. VENTING OF SOLIDS AT FULL OXIDATION RATES WITH SLURRY FLOW NEAR CAPACITY HAS ALSO BECOME A PROBLEM. VARIOUS DESIGN CHANGES ARE PROJECTED FOR THE SYSTEM DURING THE UNIT 3 FALL OUTAGE IN OCTOBER.

THE CONTINUOUS EMISSIONS MONITOR SAMPLE LINE REPLACEMENT IS NEARING COMPLETION AND SHOULD BE READY FOR TESTING IN MID-OCTOBER.

DURING THIS REPORTING PERIOD, TESTS WERE RUN ON ONE ISOLATED SCRUBBER MODULE RUNNING AT DESIGN FLOW TO DETERMINE OPERATING EFFICIENCY. RESULTS OF THESE TESTS SHOWED SOX REMOVAL RATES WITHIN DESIGN BUT ONLY WHEN LIMESTONE WAS ADDED AT A LEVEL OF OVER TWICE THE THEORETICAL STOICHIOMETRY.

10/83	3A1	22.3	39.8		21.6				
	3 A2	25.9	47.5		25.9				
	3B1	53.9	97.8		53.2				
	3B2	13.4	24.6		13.4				
	SYSTEM	38.5	69.9	69.9	38.0	744	405	283	45.3

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS OFF-LINE FROM OCTOBER 17 THROUGH THE END OF THE MONTH. PROBLEMS WITH THE DEWATERING PLANT DURING THE THIRD QUARTER WERE STILL PRESENT INTO THE FOURTH QUARTER.

ASSOCIATED ELECTRIC: THOMAS HILL 3 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS HOURS FACTOR

CARRYOVER OF SOLIDS THROUGH THE MIST ELIMINATORS CONTINUED TO BE A PROBLEM DURING OCTOBER. SLUDGE WAS BUILDING UP IN THE DUCTS AND ON THE BOTTOM OF THE STACK.

VELOCITY TESTS CONDUCTED DURING THE MONTH INDICATED ABOVE DESIGN VELOCITIES THROUGH THE MODULES. OPERATIONAL PARAMETERS WERE SET TO REDUCE VELOCITY.

DURING THE OCTOBER OUTAGE, WATER NOZZLES AND DRAINS WERE INSTALLED IN THE BREECHING DOWNSTREAM OF THE MIST ELIMINATORS AND IN THE STACK TO REDUCE SOLIDS BUILD UP.

STACK LINER DAMAGE WAS DISCOVERED TO BE THE RESULT OF CARRYOVER FROM THE FGD SYSTEM DURING THIS PERIOD. THE EXTENT OF DAMAGE IS BEING EVALUATED.

11/83	3A1	61.7	85.7		58.4				
	3A2	48.5	66.6		45.4				
	381	44.8	61.8		42.2				
	382	47.8	65.3		44.5				
	SYSTEM	67.6	93.1	93.1	63.5	720	491	457	56.3

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT OUTAGE CONTINUED THROUGH NOVEMBER 10, 1983.

FGD SYSTEM OUTAGE TIME DURING NOVEMBER WAS DUE PRIMARILY TO MIST ELIMINATOR CLEANING.

	SYSTEM	95.4	79.8	79.8	79.5	744	741	591	81.4
	3B2	84.4	67.6		67.3				
	381	91.9	75.0		74.6				
	3A2	95.7	85.8		85.4				
12/83	3 A l	14.3	11.1		11.1				

** PROBLEMS/SOLUTIONS/COMMENTS

FGD SYSTEM OUTAGE TIME DURING DECEMBER WAS DUE IN PART TO MIST ELIMINATOR CLEANING.

SEVERE COLD WEATHER CONTRIBUTED TO FGD SYSTEM DOWN TIME DURING DECEMBER.

CENTRIFUGE FAILURE TO DEWATER THE SLUDGE UNDERFLOW AT THE REQUIRED SOLIDS CONCENTRATION IS STILL A PROBLEM. NEGOTIATIONS ARE UNDERWAY WITH THE CENTRIFUGE MANUFACTURER TO PLAN PERFORMANCE GUARANTEE TESTS.

MODIFICATIONS TO THE FORCED OXIDATION SYSTEM WERE MADE DURING THE FOURTH QUARTER AND HAVE IMPROVED THE ABILITY OF THE SYSTEM TO OXIDIZE SCRUEBER SLUDGE. A NUMBER OF DESIGN AND OPERATIONAL PROBLEMS ARE CONTINUOUSLY BEING ADDRESSED.

	SYSTEM	100.0	63.3	63.3	52.6	744	619	392	53.8	
	392	74.2	21.2		17.7					
	3B1	77.4	37.6		31.3					
	3A2	97.2	73.9		61.5					
1/84	3A1	99.9	57.0		47.4					

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE EXTREME COLD WEATHER ADVERSELY EFFECTED BOTH BOILER AND SCRUBBER OPERATIONS.

2/84	3A1	95.1	48. 0	25.5
	342	66.5	53.5	28.4

ASSOCIATED ELECTRIC: THOMAS HILL 3 (CONT.)

PERIOD	MODULE	AVAILABILITY	OPERABILITY	PERFORMAN RELIABILITY	UTILIZATION	% REI	MOVAL PART.	PER HOURS	BOILER HOURS	FGD HOURS	CAP. FACTOR
	3B1 3B2 SYSTEM	67.7 65.0 98.1	60.6 62.3 74.8	88.4	32.2 33.1 39.7			696	370	276	35.3
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			HE UTILITY R EBRUARY.	EPORTED THAT	THE UNIT WAS	OFF	LINE FO	OR 13 [DAYS DUT	RING	

			DIODICT.						
3/84	3A1	73.5	68.1		65.7				
	3A2	69.2	67.8		65.4				
	3 B1	81.0	50.5		48.7				
	3B2	53.4	50. 3		48.6				
	SYSTEM	92.3	78.9	78.9	76.2	744	718	567	76.5
4/84	3A1	23.9	64.7		23.3				
	3A2	16.8	36.9		13.3				
	3B1	29.2	77.7		28.0				
	3B2	23.4	65.0		23.4				
	SYSTEM	31.1	81.4	81.4	29.4	720	260	212	28.1
	U. U. E.I.	22.2	92.7	52. 1	-/•	, _ •			

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE UNIT WAS OFF LINE 19 DAYS DURING APRIL.

THE ABSORBER AND DEWATERING FACILITIES UNDERWENT REPAIRS DURING THE MONTH.

THE UTILITY IS CONTINUING TO HAVE PROBLEMS IN THEIR ATTEMPT TO OPERATE THE DEWATERING PLANT AT REQUIRED CAPACITY FOR FULL FLUE GAS SCRUBBING. THESE PROBLEMS ARE PRIMARILY DUE TO CENTRIFUGE FAILURE AND OXIDATION SYSTEM PROBLEMS.

DURING MARCH OF THIS PERIOD, M.W. KELLOGG, THE SYSTEM SUPPLIER, CONDUCTED EXTENSIVE TESTING ON THE FGD SYSTEM. THIS TESTING WAS AN ATTEMPT TO GET THE SYSTEM OPERATING AT DESIGN SO2 REMOVAL EFFICIENCIES. AT THE END OF THE QUARTER, TESTING WAS NOT COMPLETE, BUT IT WAS FOUND THAT OVER FEEDING LIMESTONE BY 2 TO 3 TIMES WOULD RAISE THE SYSTEM PH TO LEVELS THAT WOULD GIVE REMOVAL EFFICIENCIES ABOVE 90%. OPERATION AT THIS LEVEL OF UNREACTED LIMESTONE IN THE WASTE SLURRY ONLY ADDS TO DEWATERING PROBLEMS. THROUGH THE MIDDLE OF APRIL, M.W. KELLOGG CONTINUED ITS TESTING AND WILL ASSIST THE UTILITY IN A SOLUTION TO ITS PROBLEMS WITH REACTOR CHEMISTRY.

5/84	3A1	.0	.0				
	3A2	.0	.0				
	3B1	.0	.0				
	382	.0	.0				
	SYSTEM	. 0	.0	744	0	0	. 0

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE UNIT WAS OFF LINE ALL MONTH FOR A SCHEDULED OUTAGE.

THE MODULES WERE UNAVAILABLE DUE TO REPAIR WORK IN THE ABSORBER AND DEWATERING FACILITIES.

6/84	3A1	40.0	88.0		36.9				
	3A2	40.0	88.8		37.3				
	3B1	26.3	49.5		20.8				
	3B2	20.3	42.3		17.8				
	SYSTEM	42.2	89.5	89.5	37.6	720	302	271	33.2

735

688 89.6

ASSOCIATED ELECTRIC: THOMAS HILL 3 (CONT.)

** PROBLEMS/SOLUTIONS/COMMENTS

(n

1.5

THE UTILITY REPORTED THAT THE UNIT WAS OFF LINE UNTIL JUNE 19 FOR A SCHEDULED OUTAGE.

THE ABSORBER AND DEWATERING FACILITIES WERE BEING REPAIRED DURING JUNE.

7/84	3A1	66.3	67.1	66.3	
	3A2	73.4	74.3	73.4	
	3B1	70.4	71.2	70.4	
	3B2	67.2	68.1	67.2	
	SYSTEM	92.4	93.6	92.4	744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY IS CONTINUING TO EXPERIENCE PROBLEMS IN THEIR ATTEMPT TO OPERATE THE DEWATERING PLANT AT REQUIRED CAPACITY FOR FULL FLUE GAS SCRUBBING. THOSE PROBLEMS ARE PRIMARILY DUE TO CENTRIFUGE FAILURE AND OXIDATION SYSTEM PROBLEMS.

WITH THE COMPLETION OF TESTS IN APRIL THE FGD SYSTEM SUPPLIER, M.W. KELLOGG, HAS RECOMMENDED AND WILL MAKE THE FOLLOWING MODIFICATIONS IN ATTEMPTS TO BRING THE SYSTEM UP TO DESIGN PERFORMANCE

- (1) REPLACEMENT OF REACTOR BAFFLER.
- (2) REPLACEMENT OF ALL NOZZLES WITH BETE DESIGN.
- (3) MODIFICATION OF THE RECYCLE PUMPS FOR HIGHER FLOW RATES.
- (4) INSTALL A ROUGHING DEMISTER.

THE DESCRIBED WORK IS SCHEDULED TO BEGIN AUGUST 6TH.

8/84	3A1	83.4	82.4	79.3				
	3A2	67.4	61.1	58.8				
	3B1	11.0	6.6	6.3				
	3B2	82.2	83.0	79.9				
	SYSTEM	81.3	77.7	74.8	744	716	556	86.3

** PROBLEMS/SOLUTIONS/COMMENTS

FGD SYSTEM OUTAGE TIME DURING AUGUST WAS DUE IN PART TO MODULE CLEANING.

MODULE 3B1 UNDERWENT MAJOR DESIGN MODIFICATIONS DURING AUGUST.

THE UNIT WAS DOWN DURING PART OF AUGUST DUE TO BOILER LEAKS.

FGD SYSTEM OUTAGE TIME DURING AUGUST WAS DUE IN PART TO MODULE CLEANING.

720

MODULE 3B1 UNDERWENT MAJOR DESIGN MODIFICATIONS DURING AUGUST.

THE UNIT WAS DOWN DURING PART OF AUGUST DUE TO BOILER TUBE LEAKS.

** PROBLEMS/SOLUTIONS/COMMENTS

9/84 SYSTEM

INFORMATION WAS UNAVAILABLE FOR SEPTEMBER 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COMPANY NAME PLANT NAME UNIT NUMBER CITY STATE REGULATORY CLASSIFICATION PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW NET UNIT GENERATING CAPACITY W/FGD - MW NET UNIT GENERATING CAPACITY W/FGD - MW EQUIVALENT SCRUBBED CAPACITY - MW	BASIN ELECTRIC POWER ANTELOPE VALLEY 1 BEULAH NORTH DAKOTA C 43. (.100 LB/MMBTU) 335. (.780 LB/MMBTU) 770 440 385 495 440
** UNIT DATA - BOILER AND STACK BOILER SUPPLIER BOILER TYPE BOILER SERVICE LOAD DESIGN BOILER FLUE GAS FLOW - CU.M/S BOILER FLUE GAS TEMPERATURE - C STACK HEIGHT M STACK SHELL STACK TOP DIAMETER - M	COMBUSTION ENGINEERING PULVERIZED COAL BASE 969.75 (2055000 ACFM) 154.4 (310 F) 183. (600 FT) CONCRETE 7.0 (23.0 FT)
** FUEL DATA FUEL TYPE FUEL GRADE AVERAGE HEAT CONTENT - J/G RANGE HEAT CONTENT - BTU/LB AVERAGE ASH CONTENT - % RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - % AVERAGE SULFUR CONTENT - % RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - %	COAL LIGNITE 15352. (6600 BTU/LB) 6093-7350 7.76 5.2-13.8 37.00 30.0-42.4 .68 0.4-1.2 .01 0.00-0.02
*** PARTICLE CONTROL	
** FABRIC FILTER NUMBER SUPPLIER INLET FLUE GAS CAPACITY CU.M/S INLET FLUE GAS TEMPERATURE - C PRESSURE DROP - KPA PARTICLE REMOVAL EFFICENCY - % TYPICAL GAS/CLOTH RATIO - M/MIN	1 WESTERN PREC. DIVISION, JOY 969.8 (2055000 ACFM) 85.0 (185 F) 1.0 (4.0 IN-H20) 99.8 .7 (2.2 FT/MIN)
** PARTICLE SCRUBBER NUMBER GENERIC TYPE SPECIFIC TYPE TRADE NAME/COMMON NAME SHELL GENERIC MATERIAL SHELL SPECIFIC MATERIAL LINER GENERIC MATERIAL LINER SPECIFIC MATERIAL GAS CONTACTING DEVICE TYPE *** FGD SYSTEM	0 NONE N/A N/A N/A N/A N/A
XX CENERAL DATA	
** GENERAL DATA SALEABLE PRODUCT/THROWAWAY PRODUCT SO2 REMOVAL MODE FROCESS TYPE SYSTEM SUPPLIER A-E FIRM	THROWAWAY PRODUCT SPRAY DRYING LIME/SPRAY DRYING JOY MFG/NIRO ATOMIZER STEARNS-ROGER

BASIN ELECTRIC POWER: ANTELOPE VALLEY 1 (CONT.)

```
DEVELOPMENT LEVEL
                                               FULL SCALE
   NEW/RETROFIT
                                               NEW
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - %
                                                  99.80
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                  60.00
   CURRENT STATUS
   COMMERCIAL START-UP
                                                7/84
   INITIAL START-UP
                                                5/83
   CONTRACT AWARDED
                                                8/78
** DESIGN AND OPERATING PARAMETERS
** QUENCHER/PRESATURATOR
   CONSTRUCTION MATERIAL GENERIC TYPE
                                               NR
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               NR
** ABSORBER
   NUMBER
                                                5
   NUMBER OF SPARES
                                                1
   GENERIC TYPE
                                               SPRAY DRYER
   SPECIFIC TYPE
                                               CROSSFLOW
   TRADE NAME/COMMON TYPE
                                               ROTARY ATOMIZER
   SUPPLIER
                                               JOY MFG/NIRO ATOMIZER
   DIMENSIONS - FT
                                                46.0 X 36.0
                                               CARBON STEEL
   SHELL GENERIC MATERIAL
   SHELL SPECIFIC MATERIAL
                                               ASTM A-283
   SHELL MATERIAL TRADE NAME/COMMON TYPE
                                               N/A
   LINER GENERIC MATERIAL
                                               NONE
   LINER SPECIFIC MATERIAL
                                               N/A
   LINER MATERIAL TRADE NAME/COMMON TYPE
                                               N/A
   GAS CONTACTING DEVICE TYPE
                                               NONE
   NUMBER OF CONTACTING ZONES
                                                 2
    LIQUID RECIRCULATION RATE - LITER/S
                                                               ( 100 GPM)
                                                    6.
    L/G RATIO - L/CU.M
                                                    . 0
                                                                   .2 GAL/1000 ACF)
   GAS-SIDE PRESSURE DROP - KPA
                                                   3.3
                                                              (13.3 IN-H20)
    SUPERFICAL GAS VELOCITY - M/SEC
                                                   20.4
                                                              ( 67.0 FT/S)
    INLET GAS FLOW - CU. M/S
                                                  242.56
                                                              ( 514000 ACFM)
                                                               ( 307 F)
    INLET GAS TEMPERATURE - C
                                                  152.8
    SO2 REMOVAL EFFICIENCY %
                                                  62.0
    PARTICLE REMOVAL EFFICENCY - %
                                                   99.8
** MIST ELIMINATOR
   PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                               NONE
   GENERIC TYPE
                                                N/A
   SPECIFIC TYPE
                                                N/A
    TRADE NAME/COMMON TYPE
                                                N/A
   CONSTRUCTION MATERIAL GENERIC TYPE
                                                NR
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                NR
** REHEATER
   GENERIC TYPE
                                                BYPASS
                                                COLD SIDE
    SPECIFIC TYPE
    TRADE NAME/COMMON TYPE
                                                N/A
                                                   3.2
    PERCENT GAS BYPASSED - AVG
    INLET FLUE GAS FLOW RATE - CU. M/S
                                                   31.62
                                                               ( 67000 ACFM)
                                                               ( 835 F)
    INLET FLUE GAS TEMPERATURE - C
                                                  446.1
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                NR
                                                NR
    CONSTRUCTION MATERIAL SPECIFIC TYPE
** FANS
                                                 4
   NUMBER
   DESTGN
                                                CENTRIFLIGAL
                                                COMBUSTION ENGINEERING; CEMAX
   SUPPLIER
                                                UNIT
   FUNCTION
                                                INDUCED DRAFT
   APPLICATION
   SERVICE
                                                DRY
   FLUE GAS TEMPERATURE - C
                                                               ( 185 F)
                                                  85.0
   CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL
** DAMPERS
                                                NR
   FUNCTION
   GENERIC TYPE
                                                NR
```

UTILITY FGD SURVEY: OCTOBER 1983 - SEPTEMBER 1984 BASIN ELECTRIC POWER: ANTELOPE VALLEY 1 (CONT.) NR SPECIFIC TYPE CONSTRUCTION MATERIAL GENERIC TYPE NR NR CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE NR NR LINER SPECIFIC MATERIAL TYPE ** DUCTWORK ΝR SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE NR NR LINER GENERIC MATERIAL TYPE NR LINER SPECIFIC MATERIAL TYPE ** REAGENT PREPARATION EQUIPMENT SLAKER FUNCTION BALL MILL DEVICE DEVICE TYPE N/A NUMBER (25 TPH) FULL LOAD DRY FEED CAPACITY - M. TONS/HR 22.7 PRODUCT QUALITY - % SOLIDS 38.0 ** REAGENT PREPARATION EQUIPMENT SLAKER FUNCTION DEVICE NR NR DEVICE TYPE NUMBER 1 FULL LOAD DRY FEED CAPACITY - M.TONS/HR 22.7 (25 TPH) ** TANKS NUMBER SERVICE NR ** PUMPS NUMBER SERVICE -----**** ** SOLIDS CONCENTRATING/DEWATERING NONE DEVICE *** SLUDGE ** TREATMENT N/A METHOD DEVICE N/A PROPRIETARY PROCESS N/A ** DISPOSAL NATURE FINAL TYPE LANDFILL LOCATION OFF-SITE SITE TRANSPORTATION METHOD TRUCKED SITE TREATMENT NONE ** WATER BALANCE WATER LOOP TYPE OPEN EVAPORATION WATER LOSS - LITER/S (366 GPM) 23.1 MAKEUP WATER ADDITION - LITERS/S 1.4 (22 GPM)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

5/83 SYSTEM

744

6/83 SYSTEM

720

BASIN ELECTRIC POWER: ANTELOPE VALLEY 1 (CONT.)

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT INITIAL OPERATIONS COMMENCED IN MAY 1983. THE UNIT OPERATED IN A STARTUP PHASE DURING THE MONTHS OF MAY AND JUNE.

7/83 SYSTEM 744 8/83 SYSTEM 744 9/83 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY CONTINUED PERFORMANCE TESTING ON THE FGD SYSTEM DURING THE THIRD QUARTER OF 1983.

 10/83
 SYSTEM
 744

 11/83
 SYSTEM
 720

 12/83
 SYSTEM
 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT ANTELOPE VALLEY 1 WAS STILL IN THE START-UP PHASE OF OPERATION DURING THE FOURTH QUARTER OF 1983.

 1/84
 SYSTEM
 744

 2/84
 SYSTEM
 696

 3/84
 SYSTEM
 744

 4/84
 SYSTEM
 720

 5/84
 SYSTEM
 744

 6/84
 SYSTEM
 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED TYPICAL PROBLEMS ASSOCIATED WITH START UP DURING THE PERIOD OF JANUARY THROUGH JUNE 1984.

7/84 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

COMMERCIAL OPERATION OF THE ANTELOPE VALLEY 1 FGD SYSTEM COMMENCED ON JULY 1, 1984.

8/84 SYSTEM 744 9/84 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE REPORTED FOR AUGUST AND SEPTEMBER.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

BASIN ELECTRIC POWER COMPANY NAME LARAMIE RIVER PLANT NAME UNIT NUMBER WHEATLAND CITY STATE

REGULATORY CLASSIFICATION

PARTICULATE EMISSION LIMITATION - NG/J

SO2 EMISSION LIMITATION - NG/J

NOX EMISSION LIMITATION - NG/J

NET PLANT GENERATING CAPACITY - MW

GROSS UNIT GENERATING CAPACITY - MW

STO

NET UNIT GENERATING CAPACITY W/FGD - MW

SET UNIT GENERATING CAPACITY W/FGD - MW NET UNIT GENERATING CAPACITY WO/FGD - MW
EQUIVALENT SCRUBBED CAPACITY - MW 570 ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER BABCOCK & WILCOX PULVERIZED COAL BOILER TYPE BASE DESIGN BOILER FLUE GAS FLOW - CU.M/S
BOILER FLUE GAS TEMPERATURE - C
STACK HEIGHT M BOILER SERVICE LOAD 1085.37 (2300000 ACFM) 141.1 (286 F) 183. (600 FT) CONCRETE 8.7 (28.5 FT) STACK SHELL STACK TOP DIAMETER - M ** FUEL DATA FUEL TYPE COAL FUEL GRADE SUBBITUMINOUS AVERAGE HEAT CONTENT - J/G 19538. (8400 BTU/LB) RANGE HEAT CONTENT - BTU/LB 8200-8400 7.89 AVERAGE ASH CONTENT - % 7.89 5.5-6.5 28.92 27.0-30.0 RANGE ASH CONTENT - %
AVERAGE MOISTURE CONTENT - %
RANGE MOISTURE CONTENT - %
AVERAGE SULFUR CONTENT - %
RANGE SULFUR CONTENT - % . 54 .54 0.30-0.38 RANGE SULFUR CUNTENT - /.
AVERAGE CHLORIDE CONTENT - // .04 0.01-0.02 *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER Ω TYPE NONE ** ESP NUMBER 1 NUMBER OF SPARES 0 OCOLD SIDE
BABCOCK & WILCOX
1085.4 (2300000 ACFM)
141.1 (286 F)
.8 (3. IN-H2O)
99.6 TYPE INLET FLUE GAS CAPACITY - CU.M/S
INLET FLUE GAS TEMPERATURE - C PRESSURE DROP - KPA PARTICLE REMOVAL EFFICENCY - % ** PARTICLE SCRUBBER NUMBER GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL N/A LINER GENERIC MATERIAL N/A LINER SPECIFIC MATERIAL N/A GAS CONTACTING DEVICE TYPE N/A

*** FGD SYSTEM

```
** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                             THROWAWAY PRODUCT
                                             WET SCRUBBING
   SO2 REMOVAL MODE
                                              LIMESTONE
   PROCESS TYPE
   SYSTEM SUPPLIER
                                             RESEARCH-COTTRELL
   A-E FIRM
                                              BURNS & MCDONNELL
   DEVELOPMENT LEVEL
                                              FULL SCALE
   NEW/RETROFIT
                                             NEW
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.60
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                               90.00
    ENERGY CONSUMPTION - %
   CURRENT STATUS
                                               1
    COMMERCIAL START-UP
                                               7/80
    INITIAL START-UP
                                               7/80
    CONTRACT AWARDED
                                               1/77
** DESIGN AND OPERATING PARAMETERS
    DESIGN COAL SULFER CONTENT - %
                                                  .81
                                           18931.3
    DESIGN COAL HEAT CONTENT - J/G
                                                           ( 8139 BTU/LB)
    DESIGN COAL ASH CONTENT - %
                                              7.89
    DESIGN MOISTURE CONTENT - %
                                                28.92
    DESIGN CHLORIDE CONTENT - %
                                                  .04
                                              2322.5
    SPACE REQUIREMENTS - SQ M
                                                           ( 25000 SQ FT)
    OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                80.0
** QUENCHER/PRESATURATOR
    NUMBER
                                              SPRAY ZONE
    TYPE
    SUPPLIER
                                              RESEARCH-COTTRELL
                                               271.34 ( 575000 ACFM)
141.1 ( 286 F)
    INLET GAS FLOW - CU. M/S
    INLET GAS TEMPERATURE - C
                                                           ( 9770 GPM)
    LIQUID RECIRCULATION RATE - LITERS/S
                                                           ( 17.0 GAL/1000 ACFM)
    L/G RATIO - L/CU. M
                                                2.3
    CONSTRUCTION MATERIAL GENERIC TYPE
                                             HIGH ALLOY
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                             IRON BASE/NICKEL-CHROMIUM-COPPER-MOLYBDENUM
** ARSORRER
    NUMBER
    NUMBER OF SPARES
                                               1
    GENERIC TYPE
                                              COMBINATION TOWER
                                              SPRAY/PACKED
    SPECIFIC TYPE
    TRADE NAME/COMMON TYPE
                                              N/A
                                              RESEARCH-COTTRELL
    SUPPLIER
    DIMENSIONS FT
                                              30.0 X 30.0 X 88.0
                                              STAINLESS STEEL; HIGH ALLOY
    SHELL GENERIC MATERIAL
    SHELL SPECIFIC MATERIAL
                                              AUSTENITIC; IRON BASE/NICKEL-CHROMIUM-COPPER-MOL
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                             TYPE 316L; ALLOY 904L
                                              NONE
    LINER GENERIC MATERIAL
    LINER SPECIFIC MATERIAL
                                              N/A
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                              N/A
                                              VERTICAL CROSS CHANNEL FIXED GRID PACKING
    GAS CONTACTING DEVICE TYPE
    NUMBER OF CONTACTING ZONES
                                              1
    LIQUID RECIRCULATION RATE - LITER/S
                                              1472.
                                                           (23372 GPM)
                                              5.3
    L/G RATIO - L/CU.M
                                                            ( 40.0 GAL/1000 ACF)
                                                  1.5
                                                            ( 6.0 IN-H20)
    GAS-SIDE PRESSURE DROP - KPA
    SUPERFICAL GAS VELOCITY - M/SEC
                                                 3.0
                                                            ( 10.0 FT/S)
                                               271.34
    INLET GAS FLOW - CU. M/S
                                                           ( 575000 ACFM)
                                               141.1
    INLET GAS TEMPERATURE - C
                                                            ( 286 F)
    SO2 REMOVAL EFFICIENCY - %
                                                 95.0
    PARTICLE REMOVAL EFFICENCY - %
                                                60.0
** MIST ELIMINATOR
    PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                              PRIMARY COLLECTOR
                                               5
    NUMBER PER SYSTEM
    NUMBER OF SPARES PER SYSTEM
                                               1
    NUMBER PER MODULE
                                               1
    GENERIC TYPE
                                              IMPINGEMENT
    SPECIFIC TYPE
                                              BAFFLE
    TRADE NAME/COMMON TYPE
                                             CLOSED VANE
    CONFIGURATION
                                             HORIZONTAL
```

SPECIFIC TYPE

```
NUMBER OF STAGES
   NUMBER OF PASSES PER STAGE
                                                              ( 2.6 IN-H20)
                                                    .6
   PRESSURE DROP - KPA
                                                              ( 10.0 FT/S)
    SUPERFICAL GAS VELOCITY - M/S
                                                   3.0
   CONSTRUCTION MATERIAL GENERIC TYPE
                                               ORGANIC
                                               POLYPROPYLENE
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               COOLING TOWER BLOWDOWN
   WASH WATER SOURCE
                                               UNDER-ONCE/15 MIN; TOP-ONCE/8 HRS
    WASH FREQUENCY
                                                              ( 292 GAL/MIN)
   WASH RATE - L/S
** REHEATER
                                               BYPASS
    GENERIC TYPE
                                               N/A
    SPECIFIC TYPE
    TRADE NAME/COMMON TYPE
                                               N/A
    PERCENT GAS BYPASSED - AVG
                                                  15.0
                                                                 23 F)
                                                              (
    TEMPERATURE INCREASE - C
                                                  12.8
    INLET FLUE GAS TEMPERATURE - C
                                                              ( 127 F)
                                                  52.8
                                                              ( 150 F)
                                                 65.6
    OUTLET FLUE GAS TEMPERATURE - C
                                               STAINLESS STEEL
    CONSTRUCTION MATERIAL GENERIC TYPE
                                              AUSTENITIC
    CONSTRUCTION MATERIAL SPECIFIC TYPE
** FANS
                                                2
    NUMBER
                                                0
    NUMBER OF SPARES
                                               AXIAL
    DESIGN
                                               BABCOCK & WILCOX
    SUPPLIER
    FUNCTION
                                               UNIT
                                               FORCED DRAFT
    APPLICATION
                                               DRY
    SERVICE
    FLUE GAS FLOW RATE - CU.M/S
                                                 542.68
                                                              (1150000 ACFM)
    FLUE GAS TEMPERATURE - C
                                                 141.1
                                                              ( 286 F)
                                                              (25.0 IN-H20)
    PRESSURE DROP KPA
                                                   7.6
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL
** FANS
                                                2
    NUMBER
    NUMBER OF SPARES
                                                ٥
                                               AXIAL
    DESIGN
                                               BABCOCK & WILCOX
    SUPPLIER
    FUNCTION
                                               UNIT
                                               FORCED DRAFT
    APPLICATION
    SERVICE
                                               DRY
                                               CARBON STEEL
    CONSTRUCTION MATERIAL GENERIC TYPE
** DAMPERS
                                                 4
    NUMBER
                                               CONTROL
    FUNCTION
                                                LOUVER; LOUVER
    GENERIC TYPE
                                                PARALLEL BLADE MULTILOUVRE; OPPOSED BLADE MULTIL
    SPECIFIC TYPE
                                                FORNEY ENGINEERING
    MANUFACTURER
                                               DRY SIDE-CARBON STEEL; WET SIDE-STAINLESS STEEL
    CONSTRUCTION MATERIAL GENERIC TYPE
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                AISI 1110; AUSTENITIC
    LINER GENERIC MATERIAL TYPE
                                               NONE
    LINER SPECIFIC MATERIAL TYPE
                                                N/A
** DAMPERS
    NUMBER
                                                 1
    FUNCTION
                                                CONTROL
                                                LOUVER; LOUVER
    GENERIC TYPE
    SPECIFIC TYPE
                                                PARALLEL BLADE MULTILOUVRE; OPPOSED BLADE MULTIL
    MANUFACTURER
                                                FORNEY ENGINEERING
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                DRY SIDE-CARBON STEEL; WET SIDE-STAINLESS STEEL
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                AISI 1110; AUSTENITIC
    LINER GENERIC MATERIAL TYPE
                                                NONE
    LINER SPECIFIC MATERIAL TYPE
                                                N/A
** DAMPERS
    NUMBER
                                                 2
    FUNCTION
                                                CONTROL
    GENERIC TYPE
                                                LOUVER; LOUVER
```

PARALLEL BLADE MULTILOUVRE; OPPOSED BLADE MULTIL

MANUFACTURER
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

FORNEY ENGINEERING
DRY SIDE-CARBON STEEL; WET SIDE-STAINLESS STEEL
AISI 1110; AUSTENITIC
NONE
N/A

** DAMPERS NUMBER

FUNCTION
GENERIC TYPE
SPECIFIC TYPE
MANUFACTURER
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

10
5 CONTROL & 5 SHUT-OFF
LOUVER; LOUVER
PARALLEL BLADE MULTILOUVRE; OPPOSED BLADE MULTIL
FORNEY (LOUVER); ANDCO [GUILLOTINE]
DRY SIDE-CARBON STEEL; WET SIDE-STAINLESS STEEL
AISI 1110; AUSTENITIC
NONE
N/A

** DAMPERS

NUMBER

FUNCTION
GENERIC TYPE
SPECIFIC TYPE
MANUFACTURER
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

5
SHUT-OFF
LOUVER; LOUVER
PARALLEL BLADE MULTILOUVRE; OPPOSED BLADE MULTIL
FORNEY [LOUVER]; ANDCO [GUILLOTINE]
DRY SIDE-CARBON STEEL; WET SIDE-STAINLESS STEEL
AISI 1110; AUSTENITIC
NONE
N/A

** DUCTWORK

LOCATION
CONFIGURATION
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

INLET
RECTANGULAR
CARBON STEEL
AISI 1110
NONE
N/A

** DUCTWORK

LOCATION

CONFIGURATION
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

OUTLET
RECTANGULAR
STAINLESS STEEL
AUSTENITIC
NONE
N/A

** DUCTWORK

LOCATION
CONFIGURATION
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

BYPASS RECTANGULAR CARBON STEEL AISI 1110 NONE N/A

** REAGENT PREPARATION EQUIPMENT

FUNCTION

DEVICE

DEVICE TYPE

MANUFACTURER

NUMBER

NUMBER

FULL LOAD DRY FEED CAPACITY - M.TONS/HR

PRODUCT QUALITY - % SOLIDS

WET BALL MILL
COMPARTMENTED
NR
KENNEDY VAN SAUN
2
0

13.6 (15 TPH) 35.0

** TANKS

SERVICE NUMBER
-----ABSORBER FEED 5
QUENCHER FEED 5
LIMESTONE SLURRY 1
RECLAIM WATER 1
CENTRATE 1
SEAL WATER 1

SITE TRANSPORTATION METHOD

```
** PUMPS
                                                NUMBER
    SERVICE
                                                  10
    ABSORBER FEED
                                                   5
    QUENCHER FEED
                                                   2
    MILL PRODUCT
    LIMESTONE SLURRY TRANSFER
    MAKEUP WATER SUPPLY
                                                   1
    RECLAIMED WATER
    SEAL WATER
    ABSORBER BLOWDOWN
    THICKENER UNDERFLOW
    CENTRATE
    DEWATERING BUILDING SUMP PUMPS
** SOLIDS CONCENTRATING/DEWATERING
                                                THICKENER
    DEVICE
    NUMBER
                                                3
    NUMBER OF SPARES
                                                0
                                                CIRCULAR
    CONFIGURATION
    DIMENSIONS - FT
                                                110.0 DIA X 10.0
                                                1000000
    CAPACITY
    SHELL GENERIC MATERIAL TYPE
                                               INORGANIC
                                              HYDRAULICALLY-BONDED CONCRETE
    SHELL SPECIFIC MATERIAL TYPE
                                           QUENCHER BLEED
650 GPM; 10% SOLIDS
100 GPM; 30% SOLIDS
550 GPM; 0.5% SOLIDS
TO CENTRINGE
    FEED STREAM SOURCE
    FEED STREAM CHARACTERISTICS
    OUTLET STREAM CHARACTERISTICS
    OVERFLOW STREAM CHARACTERISTICS
    OUTLET STREAM DISPOSITION
                                                TO CENTRIFUGE
    OVERFLOW STREAM DISPOSITION
                                               TO RECLAIMED WATER & THEN TO QUENCHER
** SOLIDS CONCENTRATING/DEWATERING
    DEVICE
                                                CENTRIFUGE
    NUMBER
                                                4
    NUMBER OF SPARES
                                                0
    DIMENSIONS - FT
                                                8
                                                110 GPM
    CAPACITY
    SHELL GENERIC MATERIAL TYPE
                                               STAINLESS STEEL
                                               AUSTENITIC
    SHELL SPECIFIC MATERIAL TYPE
     LINER GENERIC MATERIAL TYPE
                                                NONE
    LINER SPECIFIC MATERIAL TYPE
                                               N/A
    BELT GENERIC MATERIAL TYPE
                                               N/A
    BELT SPECIFIC MATERIAL TYPE
                                               N/A
    FEED STREAM SOURCE
                                                THICKENER UNDERFLOW
    FEED STREAM CHARACTERISTICS
                                                35% SOLIDS
     OUTLET STREAM CHARACTERISTICS
                                                70% SOLIDS
                                                TO PUG MILL
    OUTLET STREAM DISPOSITION
    OVERFLOW STREAM DISPOSITION
                                                TO CENTRATE TANK & THEN THICKENER
*** SLUDGE
    FULL LOAD SLUDGE QUANTITY - M.TONS/HR (DRY)
                                                                     .4 TPH)
                                                     . 4
                                                               (
    MOISTURE CONTENT - % TOTAL FREE WATER
                                                    30.0
    % CASO3 - DRY
                                                    8.0
    % CASO4 - DRY
                                                    90.0
    % CAOH2 - DRY
                                                     .0
    % CACO3 - DRY
                                                     2.0
** TREATMENT
    METHOD
                                                 FORCED OXIDATION
    DEVICE
                                                 SPARGER IN QUENCHER
     PROPRIETARY PROCESS
                                                 NONE
    INLET QUALITY %
                                                  10.0
** DISFOSAL
    NATURE
                                                 FINAI
    TYPE
                                                 LANDFILL
    LOCATION
                                                 ON-SITE
```

CONVEYED

SITE TREATMENT PVC LINING

60-90 FT DEEP [160 ACRES TOTAL FOR DISTOSAL] SITE DIMENSIONS 35

SITE SERVICE LIFE - YRS

** PROCESS CONTROL AND INSTRUMENTATION

PROCESS STREAM ABSORBER FEED & QUENCHER FEED

CHEMICAL PARAMETERS PH, SOLIDS, SO2 INLET, ACFM, SO2 OUTLET

PHYSICAL VARIABLES PERCENT SOLIDS; GAS FLOW

PH 5.8-6.2 IN ABSORBER; PH 4.5-5.0 IN QUENCHER; CONTROL LEVELS MONITOR TYPE GREAT LAKES [PH]; DYNASCIENCE FOR CONTROL [SO2; MONITOR LOCATION ABSORBER FEED TANK & QUENCHER; DENSITY ON PUMP

PROCESS CONTROL MANNER AUTOMATIC

PROCESS CHEMISTRY MODE FEED BACK [PH & DENSITY]

** WATER BALANCE

WATER LOOP TYPE CLOSED

EVAPORATION WATER LOSS - LITER/S (370 GPM) 23.3 POND SEEPAGE/RUNOFF WATER LOSS - LITERS/S

EFFLUENT WATER LOSS - LITERS/S .0 0 GPM)

RECEIVING WATER STREAM N/A

MAKEUP WATER ADDITION - LITERS/S 25.2 (400 GPM)

SOURCE OF MAKEUP WATER COOLING TOWER BLOWDOWN, WELLS & GRAYROCKS RESERV

** CHEMICALS AND CONSUMPTION

FUNCTION ABSORBENT NAME LIMESTONE PRINCIPAL CONSTITUENT 95% CACO3

SOURCE/SUPPLIER HOLLY SUGAR COMPANY CONSUMPTION 2000 TONS/MONTH UTILIZATION - % 90.0 POINT OF ADDITION BALL MILL

** FGD SPARE CAPACITY INDICES

ABSORBER - % 25.0 MIST ELIMINATOR - % 25.0 FAN Z . 0 BALL MILL - % . 0 EFFLUENT HOLD TANK - % 25.0 RECIRCULATION PUMP - % 25.0 33.3 THICKENER - % CENTRIFUGE - % . 0

** FGD SPARE COMPONENT INDICES

ARSORRER 1.0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR ----- ------ ------

7/80 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT BEGAN INITIAL AND COMMERCIAL OPERATIONS ON JULY 1, 1980. NO MAJOR

PROBLEMS WERE REPORTED DURING STARTUP.

8/80 SYSTEM 744

720 9/80 SYSTEM

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT IS STILL IN THE STARTUP PHASE OF OPERATIONS. NO PERFORMANCE DATA

ARE CURRENTLY AVAILABLE.

10/80 A 99.7 95.0 100.0 100.0 100.0 99.6 100.0 94.9

BASIN ELECTRIC POWER: LARAMIE RIVER 1 (CONT.)

			TY OPERABILITY F		TILIZATION	% REMOVAL SO2 PART.	PER	BOILER HOURS	FGD HOURS	CAP.
	С	100.0	99.7		95.0					
	D	21.5	22.6	100 0	21.5					
	Ε	100.0	81.4 100.0	100.0	77.5			700		
	SYSTEM	100.0	100.0	100.0	96.0		744	709	715	85.8
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			DURING OCTOBER SECTION DUE TO							
1/80	A	100.0	57.8		46.4					
	В	100.0		100.0	77.2					
	С	100.0	72.5	100.0	58.2					
	D	1.9	2. 3 98.3	100.0	1.9					
	Ε	100.0	98.3	100.0	78.9					
	SYSTEM	100.0	81.7	100.0	65.6		720	578	568	67.1
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			DURING NOVEMBER TO REPAIRS.	R THE BOILER I	AS OUT OF	SERVICE APP	ROXIMAT	ELY 120	HOURS	DUE
			DURING THE MON	TH MODULE D W.	AS OFF LINE	E 30 DAYS FOR	R REPAI	RS.		
12/80	A	19.6	21.1	100.0	19.6					
	В	100.0	94.4	100.0	87.9					
	Ċ	100.0	94.4 96.7	100.0	90.0					
	D		81.2	100.0	75.7					
	Ē	100.0	81.2 100.0	100.0 100.0	93.0					
	SYSTEM	98.8	98.4	100.0	91.5		744	693	692	87.0
	** PROBLE	EMS/SOLUT	IONS/COMMENTS							
			DURING DECEMBER							М
1/81	A	.0	THE WELDS IN TH	HE QUENCHER SI						М
1/81	A B		THE WELDS IN TH	HE QUENCHER SI	O .0					М
1/81		100.0	.0 91.3	HE QUENCHER SI	ECTION DUE					М
1/81	В	100.0	.0 91.3	100.0 100.0	.0 88.6					М
1/81	B C D E	100.0 100.0 100.0 100.0	.0 91.3 97.4 95.8 95.7	100.0 100.0 100.0 100.0 100.0	.0 88.6 94.5					М
1/81	B C D E	100.0 100.0 100.0 100.0	.0 91.3 97.4	HE QUENCHER SI 100.0 100.0 100.0 100.0	.0 88.6 94.5 93.0			DEHOLM		
1/81	B C D E SYSTEM	100.0 100.0 100.0 100.0	.0 91.3 97.4 95.8 95.7	HE QUENCHER SI 100.0 100.0 100.0 100.0	.0 88.6 94.5 93.0 92.8		N OF UD	DEHOLM	904L.	
1/81	B C D E SYSTEM	100.0 100.0 100.0 100.0	.0 91.3 97.4 95.8 95.7 95.0	100.0 100.0 100.0 100.0 100.0 100.0	.0 88.6 94.5 93.0 92.8 92.2	TO CORROSION	N OF UD 744 INTENAN	722	904L. 686	97.1
1/81	B C D E SYSTEM ** PROBLE	100.0 100.0 100.0 100.0 100.0 EMS/SOLUT	THE WELDS IN THE .0 .0 .0 .91.3 .97.4 .95.8 .95.7 .95.0 IONS/COMMENTS DURING JANUARY QUENCHER SECTION .0	HE QUENCHER SI 100.0 100.0 100.0 100.0 100.0 MODULE A WAS	.0 88.6 94.5 93.0 92.8 92.2 UNAVAILABED DUE TO CO	TO CORROSION	N OF UD 744 INTENAN	722	904L. 686	97.1
	B C D E SYSTEM ** PROBLE	100.0 100.0 100.0 100.0 100.0 EMS/SOLUT	THE WELDS IN THE .0 .0 .0 .91.3 .97.4 .95.8 .95.7 .95.0 IONS/COMMENTS DURING JANUARY QUENCHER SECTIOR .0 .0 .94.0	HE QUENCHER SI 100.0 100.0 100.0 100.0 MODULE A WAS ON THAT FAILEI	.0 88.6 94.5 93.0 92.8 92.2 UNAVAILABED DUE TO CO .0 84.2	TO CORROSION	N OF UD 744 INTENAN	722	904L. 686	97.1
	B C D E SYSTEM ** PROBLE	100.0 100.0 100.0 100.0 100.0 EMS/SOLUT	THE WELDS IN THE .0 91.3 97.4 95.8 95.7 95.0 IONS/COMMENTS DURING JANUARY QUENCHER SECTION 94.0 97.7	HE QUENCHER SI 100.0 100.0 100.0 100.0 MODULE A WAS DN THAT FAILEI 100.0 100.0	.0 88.6 94.5 93.0 92.8 92.2 UNAVAILABI D DUE TO CO .0 84.2 87.5	TO CORROSION	N OF UD 744 INTENAN	722	904L. 686	97.1
	B C D E SYSTEM ** PROBLE	100.0 100.0 100.0 100.0 100.0 EMS/SOLUT	THE WELDS IN THE .0 91.3 97.4 95.8 95.7 95.0 IONS/COMMENTS DURING JANUARY QUENCHER SECTION 94.0 97.7 97.8	HE QUENCHER SI 100.0 100.0 100.0 100.0 MODULE A WAS DN THAT FAILEI 100.0 100.0 100.0	.0 88.6 94.5 93.0 92.8 92.2 UNAVAILABED DUE TO CO .0 84.2	TO CORROSION	N OF UD 744 INTENAN	722	904L. 686	97.1
	B C D E SYSTEM ** PROBLE	100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0	THE WELDS IN THE .0 91.3 97.4 95.8 95.7 95.0 IONS/COMMENTS DURING JANUARY QUENCHER SECTION 94.0 97.7 97.8 90.7	HE QUENCHER SI 100.0 100.0 100.0 100.0 MODULE A WAS DN THAT FAILEI 100.0 100.0	.0 88.6 94.5 93.0 92.8 92.2 UNAVAILABI D DUE TO CO .0 84.2 87.5	TO CORROSION	N OF UD 744 INTENAN	722	904L. 686	97.1
	B C D E SYSTEM ** PROBLE	100.0 100.0 100.0 100.0 100.0 EMS/SOLUT	THE WELDS IN THE .0 91.3 97.4 95.8 95.7 95.0 IONS/COMMENTS DURING JANUARY QUENCHER SECTION 94.0 97.7 97.8	HE QUENCHER SI 100.0 100.0 100.0 100.0 MODULE A WAS DN THAT FAILEI 100.0 100.0 100.0	.0 88.6 94.5 93.0 92.8 92.2 UNAVAILABID DUE TO CO .0 84.2 87.5 87.6	TO CORROSION	N OF UD 744 INTENAN	722 CE ON I	904L. 686 NELDS 3	97.1
	B C D E SYSTEM ** PROBLE A B C D E SYSTEM	100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0	THE WELDS IN THE .0 91.3 97.4 95.8 95.7 95.0 IONS/COMMENTS DURING JANUARY QUENCHER SECTION 94.0 97.7 97.8 90.7	100.0 100.0 100.0 100.0 100.0 100.0 MODULE A WAS DN THAT FAILE!	.0 88.6 94.5 93.0 92.8 92.2 UNAVAILABED DUE TO CO .0 84.2 87.5 87.6 81.3	TO CORROSION	744 INTENAN THE UDD	722 CE ON I	904L. 686 NELDS 3	97.1 IN THE
	B C D E SYSTEM ** PROBLE A B C D E SYSTEM	100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0	THE WELDS IN THE .0 .0 .0 .91.3 .97.4 .95.8 .95.7 .95.0 IONS/COMMENTS DURING JANUARY QUENCHER SECTION .0 .0 .94.0 .97.7 .97.8 .90.7 .95.1	HE QUENCHER SI 100.0 100.0 100.0 100.0 MODULE A WAS DN THAT FAILEI 100.0 100.0 100.0 100.0	.0 88.6 94.5 93.0 92.8 92.2 UNAVAILABI D DUE TO CO .0 84.2 87.5 87.6 81.3 85.1	TO CORROSION LE DUE TO MA ORROSION OF	744 INTENAN THE UDD	722 CE ON I EHOLM C	904L. 686 NELDS 1 904L.	97.1 (N THE 81.2
	B C D E SYSTEM ** PROBLE A B C D E SYSTEM ** PROBLE	100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0	THE WELDS IN THE .0 91.3 97.4 95.8 95.7 95.0 IONS/COMMENTS DURING JANUARY QUENCHER SECTION .0 94.0 97.7 97.8 90.7 95.1 IONS/COMMENTS DURING FEBRUAR	HE QUENCHER SI 100.0 100.0 100.0 100.0 MODULE A WAS DN THAT FAILEI 100.0 100.0 100.0 100.0 THE HELDS IN	.0 88.6 94.5 93.0 92.8 92.2 UNAVAILABI D DUE TO CO .0 84.2 87.5 87.6 81.3 85.1	TO CORROSION LE DUE TO MA ORROSION OF	744 INTENAN THE UDD	722 CE ON I EHOLM C	904L. 686 NELDS 1 904L.	97.1 (N THE 81.2
2/81	B C D E SYSTEM ** PROBLE A B C D E SYSTEM ** PROBLE	100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0	THE WELDS IN THE .0 91.3 97.4 95.8 95.7 95.0 IONS/COMMENTS DURING JANUARY QUENCHER SECTION .0 94.0 97.7 97.8 90.7 95.1 IONS/COMMENTS DURING FEBRUAR MAINTENANCE OF	HE QUENCHER SI 100.0 100.0 100.0 100.0 MODULE A WAS DN THAT FAILEI 100.0 100.0 100.0 100.0	.0 88.6 94.5 93.0 92.8 92.2 UNAVAILABI D DUE TO CO .0 84.2 87.5 87.6 81.3 85.1	TO CORROSION LE DUE TO MA ORROSION OF	744 INTENAN THE UDD	722 CE ON I EHOLM C	904L. 686 NELDS 1 904L.	97.1 (N THE 81.2

	MODULE A	VAILABILI1	TY OPERABILITY	RELIABILITY	UTILIZATION				BOILER HOURS		
	D	100.0	99.7	100.0	97.2						
	E	100.0	94.5	100.0	96.0						
	SYSTEM	100.0	94.5 99.4	100.0	96.9			.744	725	721	96.6
	** PROBL	EMS/SOLUT	IONS/COMMENTS								
			DURING MARCH THE WELDS IN 904L.								
4/81		100.0		100.0	91.1						
	В	100.0		100.0							
	C	.0	.0		.0						
	D	100.0	99.9	100.0 100.0	99.3						
	E	100.0	99.4	100.0	98.9						
	SYSTEM	100.0	97.4	100.0	96.8			720	716	697	96.1
	** PROBL	EMS/SOLUT	IONS/COMMENTS								
			DURING APRIL THE QUENCHER							E WELDS	5 IN
5/81	A	106.0	86.7	100.0	78.2						
	В	100.0	98.0	100.0 100.0	78.2 88.4						
	С	.0	. 0		.0						
	D	100.0	98.3	100.0	88.7						
	Ē	100.0	99.3	100.0	89.6						
	SYSTEM	100.0	99.3 95.6	100.0	86.3			744	671	642	85.5
	** PROBL	EMS/SOLUT	IONS/COMMENTS								
			DURING MAY MO SECTION DUE T					ELDS OF	THE Q	UENCHE	₹
6/81	A	100.0	SECTION DUE T	O CORROSION (OF THE UDDEHO			ELDS ON	N THE Q	UENCHE	₹
6/81	A B	100.0 100.0	SECTION DUE T	CO CORROSION (OF THE UDDEHO 50.6			ELDS ON	N THE Q	UENCHE	₹
6/81	В	100.0	SECTION DUE T 51.5 98.8	TO CORROSION (100.0 100.0	50.6 97.1			ELDS ON	N THE Q	UENCHE	₹
6/81	B C	100.0 100.0	51.5 98.8 89.8	TO CORROSION (50.6 97.1 88.3			ELDS ON	1 THE Q	UENCHE	₹
6/81	B C D	100.0 100.0	51.5 98.8 89.8	TO CORROSION (50.6 97.1 88.3 66.7			ELDS ON	N THE Q	UENCHEI	?
6/81	B C	100.0 100.0 70.0 30.0	SECTION DUE T 51.5 98.8	100.0 100.0 100.0 100.0 100.0 100.0	50.6 97.1 88.3			ELDS ON		UENCHEF	
6/81	B C D E SYSTEM	100.0 100.0 70.0 30.0 100.0	51.5 98.8 89.8 67.8 27.3	100.0 100.0 100.0 100.0 100.0 100.0	50.6 97.1 88.3 66.7 26.8						
6/81	B C D E SYSTEM	100.0 100.0 70.0 30.0 100.0	51.5 98.8 89.8 67.8 27.3 83.8	100.0 100.0 100.0 100.0 100.0 100.0	50.6 97.1 88.3 66.7 26.8 82.4	OLM 90	4L. OR MAI	720 NTENANO	708	593	63.5
	B C D E SYSTEM ** PROBL	100.0 100.0 70.0 30.0 100.0	SECTION DUE TO SECTIO	100.0 100.0 100.0 100.0 100.0 100.0 100.0	50.6 97.1 88.3 66.7 26.8 82.4 N OUT OF SERVE UDDEHOLM 90	OLM 90	4L. OR MAI	720 NTENANO	708	593	63.5
	B C D E SYSTEM ** PROBL	100.0 100.0 70.0 30.0 100.0 EMS/SOLUT	SECTION DUE TO SECTION DUE TO SECTION DUE TO SECTION DUE TO SECTION SE	100.0 100.0 100.0 100.0 100.0 100.0 100.0	50.6 97.1 88.3 66.7 26.8 82.4 N OUT OF SERVE UDDEHOLM 90	OLM 90	4L. OR MAI	720 NTENANO	708	593	63.5
	B C D E SYSTEM ** PROBL	100.0 100.0 70.0 30.0 100.0 EMS/SOLUT	SECTION DUE TO SECTION DE MODULE THE QUENCHER SECTION DE TO SECTION DE MODULE THE QUENCHER SECTION DE TO SECTION DUE SECTION DUE TO SECTION DUE S	100.0 100.0 100.0 100.0 100.0 100.0 100.0	50.6 97.1 88.3 66.7 26.8 82.4 N OUT OF SERVE UDDEHOLM 90 95.5 99.0	OLM 90	4L. OR MAI	720 NTENANO	708	593	63.5
	B C D E SYSTEM ** PROBL	100.0 100.0 70.0 30.0 100.0 EMS/SOLUT	SECTION DUE TO SECTION DUE TO SECTION DUE TO SECTION DUE TO SECTION SE	100.0 100.0 100.0 100.0 100.0 100.0 100.0	50.6 97.1 88.3 66.7 26.8 82.4 N OUT OF SERVE UDDEHOLM 90 95.5 99.0 90.6	OLM 90	4L. OR MAI	720 NTENANO	708	593	63.5
	B C D E SYSTEM ** PROBL	100.0 100.0 70.0 30.0 100.0 EMS/SOLUT	51.5 98.8 89.8 67.8 27.3 83.8 IONS/COMMENTS D AND E MODUL THE QUENCHER 95.5 99.0 90.6 96.6	100.0 100.0 100.0 100.0 100.0 100.0 100.0	50.6 97.1 88.3 66.7 26.8 82.4 N OUT OF SERVE UDDEHOLM 90 95.5 99.0 90.6 96.6	OLM 90	4L. OR MAI	720 NTENANO	708	593	63.5
	B C D E SYSTEM ** PROBL	100.0 100.0 70.0 30.0 100.0 EMS/SOLUT	51.5 98.8 89.8 67.8 27.3 83.8 IONS/COMMENTS D AND E MODUL THE QUENCHER 95.5 99.0 90.6 96.6 .0	100.0 100.0 100.0 100.0 100.0 100.0 100.0	50.6 97.1 88.3 66.7 26.8 82.4 N OUT OF SERVE UDDEHOLM 90 95.5 99.0 90.6 96.6	OLM 90	4L. OR MAI	720 NTENANO DING.	708 CE ON TI	593 HE WELI	63.5 DS IN
	B C D E SYSTEM ** PROBL A B C D E SYSTEM	100.0 100.0 70.0 30.0 100.0 EMS/SOLUT	51.5 98.8 89.8 67.8 27.3 83.8 IONS/COMMENTS D AND E MODUL THE QUENCHER 95.5 99.0 90.6 96.6 .0 95.4	100.0 100.0 100.0 100.0 100.0 100.0 100.0	50.6 97.1 88.3 66.7 26.8 82.4 N OUT OF SERVE UDDEHOLM 90 95.5 99.0 90.6 96.6	OLM 90	4L. OR MAI	720 NTENANO	708 CE ON TI	593 HE WELI	63.5
	B C D E SYSTEM ** PROBL A B C D E SYSTEM	100.0 100.0 70.0 30.0 100.0 EMS/SOLUT	SECTION DUE TO SECTION SEC	100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0	50.6 97.1 88.3 66.7 26.8 82.4 N OUT OF SERVE UDDEHOLM 90 95.5 99.0 90.6 96.6 .0 95.4	VICE F	OR MAI CORRO	720 NTENANO DING. 744	708 CE ON TI 744	593 HE WELU 710	63.5 DS IN 86.9
	B C D E SYSTEM ** PROBL A B C D E SYSTEM	100.0 100.0 70.0 30.0 100.0 EMS/SOLUT	51.5 98.8 89.8 67.8 27.3 83.8 IONS/COMMENTS D AND E MODUL THE QUENCHER 95.5 99.0 90.6 96.6 .0 95.4	100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0	50.6 97.1 88.3 66.7 26.8 82.4 N OUT OF SERVE UDDEHOLM 90 95.5 99.0 90.6 96.6 95.4	VICE FOUL IS	OR MAI CORRO	720 NTENANO DING. 744	708 CE ON TI 744	593 HE WELU 710	63.5 DS IN 86.9
7/81	B C D E SYSTEM ** PROBL A B C D E SYSTEM	100.0 100.0 70.0 30.0 100.0 EMS/SOLUT	SECTION DUE TO SECTION DUE TO SECTION DUE TO SECTION DUE TO SECTION SE	100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0	50.6 97.1 88.3 66.7 26.8 82.4 N OUT OF SERVE UDDEHOLM 90 95.5 99.0 90.6 96.6 95.4	VICE FOUL IS	OR MAI CORRO	720 NTENANO DING. 744	708 CE ON TI 744	593 HE WELU 710	63.5 DS IN 86.9
7/81	B C D E SYSTEM ** PROBL A B C D E SYSTEM ** PROBL	100.0 100.0 70.0 30.0 100.0 EMS/SOLUT	SECTION DUE TO SECTION DUE TO SECTION DUE TO SECTION DUE TO SECTION. THE SECTION.	100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0	50.6 97.1 88.3 66.7 26.8 82.4 N OUT OF SERVE UDDEHOLM 90 95.5 99.0 90.6 96.6 .0 95.4	VICE FOUL IS	OR MAI CORRO	720 NTENANO DING. 744	708 CE ON TI 744	593 HE WELU 710	63.5 DS IN 86.9
7/81	B C D E SYSTEM ** PROBL A B C D E SYSTEM ** PROBL	100.0 100.0 70.0 30.0 100.0 EMS/SOLUT	SECTION DUE TO SECTION DUE TO SECTION DUE TO SECTION. THE SECTION.	100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 TAKEN OUT OF UDDEHOLM 906	50.6 97.1 88.3 66.7 26.8 82.4 N OUT OF SERVE UDDEHOLM 90 95.5 99.0 90.6 90.6 96.6 .0 95.4 SERVICE FOR 4L IS CORRODI	VICE FOUL IS	OR MAI CORRO	720 NTENANO DING. 744	708 CE ON TI 744	593 HE WELU 710	63.5 DS IN 86.9
7/81	B C D E SYSTEM ** PROBL A B C D E SYSTEM ** PROBL	100.0 100.0 70.0 30.0 100.0 EMS/SOLUT 100.0 100.0 100.0 100.0 EMS/SOLUT	SECTION DUE TO SECTION DUE TO SECTION DUE TO SECTION. THE SECTION.	100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 TAKEN OUT OF UDDEHOLM 900 100.0	50.6 97.1 88.3 66.7 26.8 82.4 N OUT OF SERVE UDDEHOLM 90 95.5 99.0 90.6 96.6 .0 95.4	VICE FOUL IS	OR MAI CORRO	720 NTENANO DING. 744	708 CE ON TI 744	593 HE WELU 710	63.5 DS IN 86.9
7/81	B C D E SYSTEM ** PROBL A B C D E SYSTEM ** PROBL	100.0 100.0 70.0 30.0 100.0 EMS/SOLUT 100.0 100.0 100.0 100.0 EMS/SOLUT	SECTION DUE TO SECTION DUE TO SECTION DUE TO SECTION. SECTION DUE TO SECTION. THE QUENCHER SECTION. THE QUENCHER SECTION. THE QUENCHER SECTION. THE GOODLE WAS SECTION. THE GOODLE WAS SECTION. THE GO.8 29.9 96.7	100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0	50.6 97.1 88.3 66.7 26.8 82.4 N OUT OF SERVE UDDEHOLM 90 95.5 99.0 90.6 96.6 .0 95.4 SERVICE FOR 4L IS CORRODO	VICE FOUL IS	OR MAI CORRO	720 NTENANO DING. 744	708 CE ON TI 744	593 HE WELU 710	63.5 DS IN 86.9

BASIN ELECTRIC POWER: LARAMIE RIVER 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS FACTOR ** PROBLEMS/SOLUTIONS/COMMENTS B AND E MODULES WERE TAKEN OUT OF SERVICE FOR MAINTENANCE ON WELDS IN THE QUENCHER SECTION. THE UDDEHOLM 904L IS CORRODING. 9/81 100.0 96.2 100.0 25.7 В .0 . 0 ۰.0 С 100.0 91.3 100.0 24.4 100.0 100.0 92.4 24.7 ח Ε 100.0 94.0 100.0 25.1 720 192 SYSTEM 100.0 94.0 100.0 25.1 181 25.6 ** PROBLEMS/SOLUTIONS/COMMENTS THE B MODULE WAS TAKEN OUT OF SERVICE FOR MAINTENANCE ON WELDS IN THE QUENCHER SECTION. THE UDDEHOLM 904L IS CORRODING. THE UNIT WAS TAKEN OUT OF SERVICE FOR AN ANNUAL OVERHAUL. 10/81 A 100.0 .0 В . 0 .0 С 100.0 .0 D 100.0 .0 Ε 100.0 . 0 SYSTEM 100.0 . 0 744 0 .0 ** PROBLEMS/SOLUTIONS/COMMENTS DURING OCTOBER THE UNIT WAS SHUTDOWN FOR SCHEDULED MAINTENANCE. 11/81 A 100.0 37.8 100.0 36.2

××	DBOBLEMS	/SOLLITTONS	/COMMENTS

.0

100.0

100.0

100.0

100.0

В

С

D

Ε

SYSTEM

DURING OCTOBER AND NOVEMBER MODULE B WAS DOWN FOR MAINTENANCE IN THE QUENCHER SECTION DUE TO CORROSION OF THE UDDEHOLM 904L.

720

689

423 40.3

. 0

72.4

56.6

69.9

59.0

12/81	A	46.8	47.1	100.0	46.8
	В	100.0	46.0	100.0	45.7
	С	69.1	69.5	100.0	69.1
	D	100.0	89.7	100.0	89.1
	Ε	100.0	61.1	100.0	60.7
	SYSTEM	100.0	78.3	100.0	77.8

. 0

75.7

59.2

73.1

63.2

100.0

100.0

100.0

100.0

EM 100.0 78.3 100.0 77.8 744 739 579 70.4

** PROBLEMS/SOLUTIONS/COMMENTS

DURING DECEMBER, MODULES A AND C WERE DOWN PART OF THE TIME FOR GENERAL MAINTENANCE.

PROBLEMS WERE ENCOUNTERED WITH THE SEAL COATING IN THE ABSORBER FEED TANK.

1/82	A	100.0	82.1	100.0	82.1				
	В	100.0	99.0	100.0	99.0				
	C	100.0	92.0	100.0	92.0				
	D	74.2	82.5	100.0	82.5				
	Ε	25.8	9.9	100.0	9.9				
	SYSTEM	100.0	91.4	100.0	91.4	744	744	680	85.2

			TY OPERABILITY	PERFORMANCE RELIABILITY UTI	LIZATION	% REI	10VAL PART.	PER HOURS	BOILER HOURS	FGD HOURS	FACTO
	** PRO	BLEMS/SOLUT	IONS/COMMENTS								
			DURING JANUAR	THE D AND E AB	SORBER FEE	ED TAI	K WAS	DOWN F	OR SEA	L COAT	ING.
2/82	Δ	100.0	51.2	100 0	40.4						
E/ 0E	B	100.0	89.0	100 0	70 1						
	Č	100.0	95.0	100.0	74.8						
	D	100.0	92.8								
	Ē	53.6	92.8 22.9	100.0	73.1 18.1						
	SYSTEM		82.8		69.1			672	529	465	76.2
	** PRO	BLEMS/SOLUT:	IONS/COMMENTS								
			MODULE E WAS (OFF-LINE PART OF	FEBRUARY	то м	AKE REI	PAIRS T	O THE	POTENT	AL
3/82		74.2			55.6						
	В	100.0	61.7 60.4	100.0	61.7						
	С		60.4	100.0	60.4						
	ם	100.0			98. 0						
	Ε	100.0	99.9	100.0	99.9						
	SYSTEM	100.0	93.9	100.0	93.9			744	744	699	76.1
	** PRO	BLEMS/SOLUT	IONS/COMMENTS								
				MODULE A WAS DOW M CORROSION OF 1				N THE G	UENCHE	R SECT	TON
4/82	A	50.0	65.4	100.0	25.8	.,					
•-	В	76.7	65.4 100.0	100.0 100.0	71.8						
	c	76.7		100.0	74.9						
	פ	50.0	65.4		47.0						
	E		100.0		76.1						
	SYSTEM		100.0	100.0	73.9			720	550	532	59.3
	** PRO	BLEMS/SOLUT	IONS/COMMENTS								
				MODULES B, C, D; N THE MIXERS AND					E TIME	TO PER	RFORM
			MAINTENANCE U	N INE HIXEKS AND) 10 INSPE	CI IN	E MODO	LES.			
5/82		100.0		100.0							
	В	96.8	90.3		63.2						
	С	96.8	93.3	100.0							
	D	.0	.0		. 0						
	Ε	100.0	72.5	100.0	50.8						
	SYSTEM	98.4	81.7	100.0	57.2			744	521	426	75.7
	** PRO	BLEMS/SOLUT	IONS/COMMENTS								
			MODULE D WAS	DOWN DURING MAY	FOR GENER	AL MA	INTENA	NCE AND	REPAI	R.	
6/82	A	100.0	56.6	100.0	39.1						
	_	300 -	00.7	100 0	/ T O						

** PROBLEMS/SOLUTIONS/COMMENTS

.0

100.0

100.0

100.0

100.0

92.3

84.2

.0

76.3

77.3

В

С

D

Ε

SYSTEM

DURING JUNE MODULE D WAS OUT OF SERVICE FOR NOZZLE REPAIR IN THE QUENCHER SECTION.

720 498

385 56.8

63.8

58.2

52.8

53.5

.0

100.0

100.0

100.0

100.0

BASIN ELECTRIC POWER: LARAMIE RIVER 1 (CONT.)

				PERFORMA	NCE DATA						
PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% RE	PART.	HOURS	BOILER HOURS	HOURS	CAP.
7/82	A	64.5	30.0	100.0	27.1						
	В	71.0	58.4	100.0	52.8						
	С	93.5	86.7	100.0	78 · 3						
	D	67.7	61.6	100.0	55.7						
	E	100.0	95.9	100.0	27.1 52.8 78.3 55.7 86.6 75.1			744	672	559	62.6
	SYSTEM	99.2	83.2	100.0	75.1			,,,,	0,2	337	04.0
	** PRO	BLEMS/SOLUTIO									
			URING JULY MO ECTION.	DDULES A, B	AND D WERE DO	OT NW	REPAI	R NOZZ	LES IN	THE QUE	ENCHER
8/82	A	100.0	90.2	100.0 100.0	67.3						
	В	100.0	96.3	100.0	71.8						
	С	77.4	80.5	100.0 100.0	60.0 62.8						
	D	100.0	84.1	100.0	62.8						
	E	12.9	10.3 90.4	100.0	7.7			766	555	E01	40 (
	SYSTEM	97.6	90.4	100.0	67.4			/44	555	201	00.4
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
					ND E WERE DOW PRROSION OF TH				IN THE	QUENC	IER
9/82	A	100.0	92.6 98.0	100.0	92.6						
	В		98 .0	100.0	98.0						
	C	16.7	16.6	100.0	16.6						
	D	100.0	86. 0	100.0	್ರ 86.0						
	Ε		60.0	100.0	60.0						
	SYSTEM	100.0	88.3	100.0	88.3			720	720	636	66.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
					WAS DOWN FOR			E IN T	HE QUEN	CHER SI	ECTION
10/82	Δ	100.0	86.1	100.0	49.9						
10, 01	В	16.1	10.2	100.0	5.9						
	Č	87.1	70.5	100.0	40.8						
	D	71.0	94.2	100.0	54.6						
		100.0		100.0	44.2						
		93.5						744	431	363	52.2
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
					, C AND D WERE						
11/82	A	63.3	44.3	100.0	44.3						
	В	92.9	73.3	100.0	73.3						
	C	100.0	90.8	100.0	90.8						
	D	46.7	23.8	100.0	23.8						
	E	100.0	82.7	100.0	82.7						
	SYSTEM	100.0	78.7	100.0	78.7			720	720	567	56.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
					A, B AND D WEI ULTING FROM C						S IN
12/82	A	93.5	70.0	100.0	57.4						
12/02	B	100.0	70.0 79.5	100.0	65.2						
	J	100.0	17.5	100.0	93.2						

BASIN ELECTRIC POWER: LARAMIE RIVER 1 (CONT.)

ERIOD	MODULE AV		OPERABILITY	RELIABILITY	UTILIZATION				BOILER HOURS		
	C		-32.7	100.0	26.8						
	D	100.0	43.9	100.0	36.0						
	E	96.8	57.2	100.0	46.9						
	SYSTEM	100.0	70.8	100.0	58.1			744	610	432	43.4
	** PROBLE	EMS/SOLUTIO	NS/COMMENTS								
			URING DECEMB IXERS.	ER MODULE A	WAS DOWN FOR	MAINT	ENANCE	ON THE	QUENC	HER TO	4ER
1/83			46.1								
	В	100.0	57.5 .0	100.0	52.0						
	С	74.2	.0		. 0						
	D	100.0	99.4 100.1	100.0	89.9						
	E	100.0	100.1	100.0	90.6						
	SYSTEM	100.0	75.8	100.0	68.5			744	673	510	46.2
	** PROBLI	EMS/SOLUTIO	NS/COMMENTS								
			URING JANUAR		AS DOWN FOR	MAINTE	NANCE 1	ON THE	ICI AB	SORBER	FEED
2/83	A	100.0	79.2	100.0	72.9						
	В	100.0	88.6	100.0	81.5						
	С	71.4	47.1	100.0	43.3						
	ם	71.4 39.3	47.1 38.5	100.0 100.0	43.3 35.4						
	E	100.0	83.5	100.0	76.8						
	SYSTEM	100.0	83.5 84.2	100.0	77.5			672	618	521	56.9
	** PROBL	EMS/SOLUTIO	NS/COMMENTS								
			URING FEBRUA			TO A	LEAK I	N THE C	NENCHE	R FLOOR	₹.
3/83	A		55.3								
	В	71.0	67.0	100.0	67.0						
	С	100.0	100.0	100.0	100.0						
	D	74.2	69.0	100.0	69.0						
	Ε	100.0	69.7	100.0	69.7						
	SYSTEM	100.0	100.0 69.0 69.7 90.2	100.0	90.2			744	744	671	66.0
	** PROBL	EMS/SOLUTIO	NS/COMMENTS								
			HE UTILITY R PURING MARCH.	EPORTED THAT	NO MAJOR FO	D-RELA	TED PR	OBLEMS	WERE E	NCOUNT	ERED
4/83	A	99.9	78.3	100.0	60.1						
	В	69.9	58.0	100.0	44.5						
	С	99. 9	92.5	100.0	71.0						
	D	99.9	81.7	100.0	62.7						
	Ε	33.3	8.3	100.0	6.4						
	SYSTEM	100.0	79.7	100.0	61.2			720	553	441	57.0
	** PROBL	EMS/SOLUTIO	NS/COMMENTS								
			NODULE E WAS NUENCHER TOWE		APRIL FOR MA	AINTENA	NCE, C	LEANIN	G AND P	ACKING	OF THE
5/83	A	41.9	97.3	100.0	40.6						
	B	41.9	94.6	100.0	39.4						
	C	41.9	92.8	100.0	38.7						
		41.9	92. 0 98.9		30.7 41.2						
	D			100.0							
	E	.0	.0	100.0	.0			744	710	^^-	00 0
	SYSTEM	41.9	95.9	100.0	40.0			744	310	297	80.3

BASIN ELECTRIC POWER: LARAMIE RIVER 1 (CONT.)

ERIOD	MODULE A		ITY OPERABILITY R			SO2 PART.	HOURS			
	** PROBL	EMS/SOLUT	TIONS/COMMENTS							
			THE UNIT WAS DO	NWN DURING PAR	T OF MAY	FOR AN ANNUA	L OUTAG	E.		
6/83	A	.0			.0					
	В	.0			. 0					
	c	.0			.0					
	E	.0			.0					
	D System	.0			.0 .0		720	0	0	.0
	** PROBL	EMS/SOLUT	TIONS/COMMENTS							
			ALL MODULES WER	E DOWN DURING	JUNE FOR	MAINTENANCE	AND AN	ANNUAL	OVERH	IAUL.
7/83	A	22.6	18.5	100.0	9.8					
	В	58.1	2.8							
	С	61.3	96.4	100.0 100.0	1.5 51.2					
	D	83.9	98.4 93.6	100.0	52.3					
	E	47.8	93.6	100.0	49.7					
	SYSTEM	68.4	77.4	100.0	41.1		744	395	306	55.5
	** PROBLE	EMS/SOLUT	TIONS/COMMENTS							
			MODULES A, B, C	, D, AND E WE	RE DOWN FO	OR MAINTENANO	E DURI	NG PART	OF JU	ILY.
8/83		100.0		100.0	50.5					
	В	83.9	50.1	100.0	46.0					
	C	100.0			70.5					
	D	87.1		100.0	54.9					
	E System	100.0			77.4 74.8		744	683	557	56 6
	** PROBLE		IONS/COMMENTS				744	003	337	20.0
			MODULES B AND D	WERE DOWN DIE	DING DADT	OF AUGUST FO	1D MATA	TENANCE		
9/83		100.0				01 X00031 FC	K HAIN	TENANCE	•	
7/03	В	100.0	88.1	100.0	88.1					
	C	100.0 86.7	59.5		59.5					
	Č	86.7	81.0 81.0		81.0					
	Ď	10.0	91.0	100.0	81.0					
	E	100.0			91.0					
	SYSTEM	96.7		100.0	63.7 92.9		720	720	669	80.7
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			MODULE C WAS DO	WN DURING PAR	T OF SEPTE	MBER FOR MAI	NTENAN	CE REQU	IRED O	N THE
1/07		47 -	QUENCHER SECTIO			LITYER AKOBIE	ns.			
0/83	В	67.7	45.8	100.0	39.5					
	C	100.0	80.6	100.0	69.5					
	ם	55.0 100.0	54.0	100.0	46.6					
	Ε	100.0	66.9	100.0	57.7					
	SYSTEM	100.0	91 .9 84.8	100.0 100.0	79.3 73.2		744	642	544	70.9
	** PROBLE	MS/SOLUT	IONS/COMMENTS				. , ,	J . L	314	. • • •

11/83 A 80.0 60.8 100.0 60.8

PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% REI 502	10VAL PART.	PER HOURS	BOILER HOURS	FGD HOURS	FACTOR
	В	100.0		100.0 100.0 100.0							
	С	100.0	97.4	100.0	97.4						
	D	43.3	34.9	100.0	34.9						
	Ε	100.0	83.9	100.0	83.9						
	SYSTEM	100.0 100.0	86.7	100.0	86.7			720	720	624	70.8
12/83	A		89.0	100.0							
	В	100.0	85.3	100.0	79.0						
	С	100.0 100.0	44.7	100.0 100.0	41 4						
	D	64.5	51.6	100.0	47.8						
	Ε	100.0	55.4	100.0	51.3						
	SYSTEM	100.0	81.5	100.0	75.5			744	689	561	69.3
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			HE UTILITY R		NO MAJOR FGD BER 1983.	-RELA	TED PR	OBLEMS	WERE E	NCOUNTI	ERED
1/84	A	80.6	54.0	100.0	49.6						
-, -	В	80.6 100.0	54.0 82.7	100.0 100.0	76.0						
	Ċ	100.0	42 4	100.0	39.0						
	D	100.0 100.0	57.2	100.0 100.0	39.0 52.6						
	Ē	100.0	77 7	100.0	71 4						
	SYSTEM		78.5	100.0	72.2			744	684	537	62.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			-	DOWN FOR MAI	NTENANCE OF 1	TANK M	IXERS	AND REI	PAIR OF	A FEE)
	.3		UMP.								
2/84	A	89.7	71.7	100.0	66.1						
	В	100.0	51.1 13.6	100.0 100.0	47.1						
	С	13.8	13.6	100.0	12.6						
	D	100.0	80.5	100.0	74.3						
	Ε	100.0	86.5	100.0 100.0	79.8						
	SYSTEM	100.0						696	642	487	59.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			HE UTILITY R EBRUARY.	EPORTED THAT	MODULE C WAS	S DOWN	FOR M	AINTEN	ANCE DU	RING	
3/84	A	F				DOWN	FOR M	AINTEN	ANCE DU	RING	
3/84	A B	100.0	EBRUARY. 89.8	100.0		S DOWN	FOR M	AINTEN	ANCE DU	RING	
3/84	В	100.0 100.0	89.8 95.4	100.0 100.0	87.7 93.1	S DOWN	FOR M	AINTEN	ANCE DU	RING	
3/84	B C	100.0 100.0 93.5	89.8 95.4 45.2	100.0 100.0 100.0	87.7 93.1 44.1	S DOWN	FOR M	AINTEN	ANCE DU	RING	
3/84	B C D	100.0 100.0 93.5 9.7	89.8 95.4 45.2 3.4	100.0 100.0 100.0 100.0	87.7 93.1 44.1 3.3	S DOWN	FOR M	AINTEN	ANCE DU	RING	
3/84	B C	100.0 100.0 93.5 9.7 100.0	89.8 95.4 45.2	100.0 100.0 100.0	87.7 93.1 44.1	5 DOMN	FOR M	AINTEN			60.5
3/84	B C D E SYSTEM	100.0 100.0 93.5 9.7 100.0	89.8 95.4 45.2 3.4 83.1 79.2	100.0 100.0 100.0 100.0 100.0	87.7 93.1 44.1 3.3 81.1	S DOMN	FOR M				60.5
3/84	B C D E SYSTEM	F 100.0 100.0 93.5 9.7 100.0 100.0 BLEMS/SOLUTIO	89.8 95.4 45.2 3.4 83.1 79.2 NS/COMMENTS	100.0 100.0 100.0 100.0 100.0	87.7 93.1 44.1 3.3 81.1			744	726	575	
3/84	B C D E SYSTEM	F 100.0 100.0 93.5 9.7 100.0 100.0 BLEMS/SOLUTIO	89.8 95.4 45.2 3.4 83.1 79.2 NS/COMMENTS	100.0 100.0 100.0 100.0 100.0	87.7 93.1 44.1 3.3 81.1 77.3			744	726	575	
	B C D E SYSTEM	F 100.0 100.0 93.5 9.7 100.0 100.0 BLEMS/SOLUTIO	89.8 95.4 45.2 3.4 83.1 79.2 NS/COMMENTS	100.0 100.0 100.0 100.0 100.0 100.0	87.7 93.1 44.1 3.3 81.1 77.3			744	726	575	
	B C D E SYSTEM ** PRO	F 100.0 100.0 93.5 9.7 100.0 100.0 T 99.9	89.8 95.4 45.2 3.4 83.1 79.2 NS/COMMENTS HE UTILITY R	100.0 100.0 100.0 100.0 100.0 100.0	87.7 93.1 44.1 3.3 81.1 77.3			744	726	575	
	B C D E SYSTEM ** PRO	F 100.0 100.0 93.5 9.7 100.0 100.0 BLEMS/SOLUTIO T 99.9 20.0 99.9	89.8 95.4 45.2 3.4 83.1 79.2 NS/COMMENTS HE UTILITY R 97.2 7.2 88.6	100.0 100.0 100.0 100.0 100.0 100.0	87.7 93.1 44.1 3.3 81.1 77.3 MODULE D WAS 93.1 6.9 84.9			744	726	575	
	B C D E SYSTEM ** PROD	F 100.0 100.0 93.5 9.7 100.0 100.0 BLEMS/SOLUTIO T 99.9 20.0	89.8 95.4 45.2 3.4 83.1 79.2 NS/COMMENTS HE UTILITY R 97.2 7.2	100.0 100.0 100.0 100.0 100.0 100.0	87.7 93.1 44.1 3.3 81.1 77.3 MODULE D WAS			744	726	575	

BASIN ELECTRIC POWER: LARAMIE RIVER 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS FACTOR ** PROBLEMS/SOLUTIONS/COMMENTS MODULE B WAS DOWN FOR MECHANICAL MAINTENANCE DURING APRIL. MODULE D WAS DOWN FOR MECHANICAL REVISIONS OF ABSORBER TANK MIXERS. 5/84 100.0 97.0 100.0 97.0 ₿ 71.0 65.2 100.0 65.2 С 84.2 100.0 84.2 100.0 Ð 100.0 79.7 100.0 79.7 F 32.3 27.0 100.0 27.0 SYSTEM 100.0 88.3 100.0 744 744 657 67.4 88.3 ** PROBLEMS/SOLUTIONS/COMMENTS MODULES B AND E WERE DOWN DURING MAY FOR MAINTENANCE. 6/84 53.3 62.2 100.0 9.9 В 53.3 . 0 .0 С 46.7 83.5 100.0 13.3 D 100.0 79.0 100.0 12.6 F 46.7 92.6 100.0 14.8 SYSTEM 75.0 79.3 100.0 12.7 720 115 91 50.2 ** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT MODULES A, C, D AND E WERE OUT FOR TANK MIXER REPAIRS. 7/84 Δ . 0 . 0 . 0 В 100.0 94.8 100.0 90.7 С 100.0 51.9 100.0 49.7 ח 100.0 86.9 100.0 83.2 Ε 100.0 84.6 100.0 81.0 SYSTEM 100.0 79.6 100.0 76.1 744 712 566 58.6 ** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS AROSE DURING JULY. 8/84 Α 71.0 45.5 100.0 45.3 В 74.2 71.7 100.0 71.4 С 71.0 69.1 100.0 68.8 D 100.0 79.4 100.0 79.0 Ε 100.0 75.0 100.0 74.7 SYSTEM 100.0 85.1 100.0 84.8 744 741 631 61.3 ** PROBLEMS/SOLUTIONS/COMMENTS

MODULES A,8 AND C WERE DOWN DURING PART OF AUGUST FOR TANK MIXER REPAIRS.

9/84 SYSTEM

720

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR SEPTEMBER 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COMPANY NAME BASIN ELECTRIC POWER LARAMIE RIVER PLANT NAME UNIT NUMBER WHEATLAND CITY WYOMING STATE REGULATORY CLASSIFICATION Δ (.100 LB/MMBTU) (.200 LB/MMBTU) 43. 86. PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J (**** LB/MMBTU) ***** NOX EMISSION LIMITATION - NG/J 1500 NET PLANT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW 570 NET UNIT GENERATING CAPACITY W/FGD - MW 500 NET UNIT GENERATING CAPACITY WO/FGD - MW 495 FQUIVALENT SCRUBBED CAPACITY - MW 570 ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER BABCOCK & WILCOX BOILER TYPE PULVERIZED COAL BOILER SERVICE LOAD BASE DESIGN BOILER FLUE GAS FLOW - CU.M/S 1321.32 (2800000 ACFM) 56.1 (133 F) BOILER FLUE GAS TEMPERATURE - C STACK HEIGHT - M 183. (600 FT) STACK SHELL CONCRETE (28.6 FT) STACK TOP DIAMETER - M 8.7 ** FUEL DATA FUEL TYPE COAL FUEL GRADE SUBBITUMINOUS AVERAGE HEAT CONTENT - J/G 19538. (8400 BTU/LB) RANGE HEAT CONTENT - BTU/LB ***** AVERAGE ASH CONTENT - % 7.89 RANGE ASH CONTENT - % ***** AVERAGE MOISTURE CONTENT - % 28.92 RANGE MOISTURE CONTENT - % ***** AVERAGE SULFUR CONTENT - % .54 RANGE SULFUR CONTENT - % 0.2-0.8 AVERAGE CHLORIDE CONTENT - % .04 RANGE CHLORIDE CONTENT - % *** PARTICLE CONTROL ** ESP NUMBER COLD SIDE TYPE SUPPLIER BABCOCK & WILCOX INLET FLUE GAS CAPACITY - CU.M/S 1085.4 (2300000 ACFM) 141.1 (286 F) (3. IN-H20) INLET FLUE GAS TEMPERATURE - C .8 PRESSUPE DROP - KPA .8 99.6 PARTICLE REMOVAL EFFICENCY - % ** PARTICLE SCRUBBER NUMBER a GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL N/A LINER GENERIC MATERIAL N/A LINER SPECIFIC MATERIAL N/A GAS CONTACTING DEVICE TYPE N/A *** FGD SYSTEM ** GENERAL DATA SALEABLE PRODUCT/THROWAWAY PRODUCT THROWAWAY PRODUCT SO2 REMOVAL MODE WET SCRUBBING PROCESS TYPE LIMESTONE SYSTEM SUPPLIER RESEARCH-COTTRELL

BURNS & MCDONNELL

A-E FIRM

BASIN ELECTRIC POWER: LARAMIE RIVER 2 (CONT.)

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DEVELOPMENT LEVEL FULL SCALE
NEW/RETROFIT
UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.60
UNIT DESIGN SO2 REMOVAL EFFICIENCY - % 90.00
CURRENT STATUS
COMMERCIAL START-UP 7/86
INITIAL START-UP 7/81
CONTRACT AWARDED 1/77
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** DESIGN AND OPERATING PARAMETERS

** QUENCHER/PRESATURATOR

CONSTRUCTION MATERIAL GENERIC TYPE NR
CONSTRUCTION MATERIAL SPECIFIC TYPE NR

** ABSORBER

NUMBER COMBINATION TOWER GENERIC TYPE SPECIFIC TYPE SPRAY/PACKED TRADE NAME/COMMON TYPE N/A RESEARCH-COTTRELL SUPPLIER 30.0 X 30.0 X 88.0 DIMENSIONS - FT STAINLESS STEEL; HIGH ALLOY SHELL GENERIC MATERIAL AUSTENITIC; IRON BASE/NICKEL-CHROMIUM-COPPER-MOL SHELL SPECIFIC MATERIAL SHELL MATERIAL TRADE NAME/COMMON TYPE TYPE 316L; ALLOY 904L LINER GENERIC MATERIAL NONE LINER SPECIFIC MATERIAL N/A LINER MATERIAL TRADE NAME/COMMON TYPE N/A GAS CONTACTING DEVICE TYPE VERTICAL CROSS CHANNEL FIXED GRID PACKING NUMBER OF CONTACTING ZONES DISTANCE BETWEEN GAS CONTACTING ZONES - CM 61.0 24.0IN) L/G RATIO L/CU.M (60.0 GAL/1000 ACF) 8.0 SUPERFICAL GAS VELOCITY M/SEC 3.0 (10.0 FT/S) INLET GAS FLOW - CU. M/S 1085.37 (2300000 ACFM) INLET GAS TEMPERATURE - C 141.1 (286 F) SO2 REMOVAL EFFICIENCY % 90.0 PARTICLE REMOVAL EFFICENCY - % . 0

** MIST ELIMINATOR

PRE-MIST ELIMINATOR/MIST ELIMINATOR PRIMARY COLLECTOR GENERIC TYPE IMPINGEMENT SPECIFIC TYFE BAFFLE TRADE NAME/COMMON TYPE CLOSED VANE VERTICAL CONFIGURATION NUMBER OF STAGES 1 NUMBER OF PASSES PER STAGE 1 CONSTRUCTION MATERIAL GENERIC TYPE ΝP CONSTRUCTION MATERIAL SPECIFIC TYPE ΝR

** REHEATER

GENERIC TYPE NONE
SPECIFIC TYPE N/A
TRADE NAME/COMMON TYPE N/A
CONSTRUCTION MATERIAL GENERIC TYPE NONE
CONSTRUCTION MATERIAL SPECIFIC TYPE N/A

** FANS

NUMBER 2
DESIGN CENTRIFUGAL
FUNCTION UNIT
APPLICATION FORCED DRAFT
SERVICE DRY
CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL

** FANS

NUMBER OF SPARES 0

DESIGN AXIAL
SUPPLIER BABCOCK & WILCOX
FUNCTION UNIT
APPLICATION FORCED DRAFT

BASIN ELECTRIC POWER: LARAMIE RIVER 2 (CONT.)

SERVICE DRY CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL

** DAMPERS

FUNCTION NΡ GENERIC TYPE NR SPECIFIC TYPE ND CONSTRUCTION MATERIAL GENERIC TYPE NR NR CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE NR LINER SPECIFIC MATERIAL TYPE NR

** DUCTWORK

SHELL GENERIC MATERIAL TYPE NR SHELL SPECIFIC MATERIAL TYPE NR LINER GENERIC MATERIAL TYPE NR LINER SPECIFIC MATERIAL TYPE NR

** REAGENT PREPARATION EQUIPMENT

FUNCTION WET BALL MILL DEVICE COMPARTMENTED DEVICE TYPE NR NUMBER FULL LOAD DRY FEED CAPACITY - M.TONS/HR 13.6

(15 TPH) PRODUCT QUALITY - % SOLIDS 30.0

** TANKS

SERVICE NUMBER NΩ ****

** PUMPS

SERVICE NUMBER ----------****

** SOLIDS CONCENTRATING/DEWATERING

DEVICE THICKENER NUMBER 3 NUMBER OF SPARES n DIMENSIONS FT 110.0 DIA X 10.0 SHELL GENERIC MATERIAL TYPE INORGANIC SHELL SPECIFIC MATERIAL TYPE HYDRAULICALLY-BONDED CONCRETE

** SOLIDS CONCENTRATING/DEWATERING

DEVICE CENTRIFUGE NUMBER 1 NUMBER OF SPARES Ω FEED STREAM CHARACTERISTICS 35% SOLIDS OUTLET STREAM CHARACTERISTICS 60% SOLIDS

*** SLUDGE

** TREATMENT FORCED OXIDATION METHOD DEVICE OXIDATION TANK

PROPRIETARY PROCESS N/A

** DISPOSAL NATURE TYPE

LANDFILL ON-SITE LOCATION SITE TRANSPORTATION METHOD CONVEYED SITE TREATMENT NONE SITE SERVICE LIFE - YRS 35

** PROCESS CONTROL AND INSTRUMENTATION

CHEMICAL PARAMETERS PH, SOLIDS, SO2 INLET, ACFM, SO2 OUTLET PROCESS CONTROL MANNER AUTOMATIC

FINAL

BASIN ELECTRIC POWER: LARAMIE RIVER 2 (CONT.)

** WATER BALANCE

CLOSED WATER LOOP TYPE

16.9 (269 GPM) MAKEUP WATER ADDITION - LITERS/S

		AVAILABILITY	OPERABILITY		UTILIZATION	% REM 502	OVAL PART.	PER HOURS	HOURS	FGD HOURS	CAP.
7/01	SYSTEM							744			
// 01								, , , ,			
	** PRO	BLEMS/SOLUTIO									
		I	NITIAL OPERA	TION OF THE F		GAN DU	RING .	JULY 19	981.		
8/81	A	100.0	78.2	100.0 100.0	77.6						
	В	52.4	52.8	100.0	52.4						
	C	100.0	82.3 32.2 28.8 68.6	100.0	81.7						
	D	31.9	32.2	100.0	31.9						
	E	100.0	28.8	100.0	28.6			7//	738	F 6 /	
	SYSTEM	96.1	68.6	100.0	68.1			/44	/38	506	46.7
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
				S WERE OUT O		THAT	BRACIN	NG WORK	ON ROL	JND-0F F	:
9/81	A	100.0	94.0	100.0	77.4						
- -	В	100.0	99.0	100.0	81.5						
	Č	37.7	31.2	100.0	25.7						
	D	100.0	41.7	100.0	34.3						
	Ē		60.4	100.0	49.7						
	SYSTEM		81.6	100.0	67.2			720	593	483	55.7
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			HE UTILITY RI	EPORTED NO PR	OBLEMS WITH	THE FG	D S YS1	rem wer	RE ENCOL	NTEREC	IN
10/81	Δ	97 0	78 9	100.0	70 1						
10,01	B	100.0	99.1	100.0	98.1						
	Č	100.0	99.2	100.0	98.2						
	D	100.0	96.0		94.9						
	Ē	38.7	11.7	100.0 100.0							
					11 /						
	5151EM		96.2		11.6 95.0			744	736	708	88.0
			96.2					744	736	708	88.0
		100.0 BLEMS/SOLUTIO	96.2 NS/COMMENTS		95.0	F-LINE	PART				88.0
		100.0 BLEMS/SOLUTIO	96.2 NS/COMMENTS URING OCTOBER	100.0	95.0 ND A WERE OF	F-LINE	PART				88.0
11/81	** PROD	100.0 BLEMS/SOLUTIO	96.2 NS/COMMENTS URING OCTOBER HE INSTALLAT	100.0 R MODULES E A ION OF BRACIN	95.0 ND A WERE OF G.	F-LINE	PART				88.0
11/81	** PROD	100.0 BLEMS/SOLUTIO D T	96.2 NS/COMMENTS URING OCTOBER HE INSTALLAT	100.0 R MODULES E A ION OF BRACIN 100.0	95.0 ND A WERE OF G. 99.9	F-LINE	PART				88.0
11/81	** PROS	100.0 BLEMS/SOLUTIO D T 100.0	96.2 NS/COMMENTS URING OCTOBER HE INSTALLAT 99.9	100.0 R MODULES E A ION OF BRACIN	95.0 ND A WERE OF G. 99.9 99.9	F-LINE	PART				88.0
11/81	** PROS	100.0 BLEMS/SOLUTIO D T 100.0 100.0	96.2 NS/COMMENTS URING OCTOBER HE INSTALLAT 99.9 99.9	100.0 R MODULES E A ION OF BRACIN 100.0 100.0	95.0 ND A WERE OF G. 99.9 99.9 99.9	F-LINE	PART				88.0
11/81	** PROD A B C D E	100.0 BLEMS/SOLUTIO T 100.0 100.0 100.0 100.0	96.2 NS/COMMENTS URING OCTOBER HE INSTALLAT 99.9 99.9 99.9 94.0 .0	100.0 R MODULES E A ION OF BRACIN 100.0 100.0 100.0 100.0	95.0 ND A WERE OF G. 99.9 99.9 99.9 94.0 .0	F-LINE	PART	OF THE	E TIME P	FOR	
11/81	** PROD	100.0 BLEMS/SOLUTIO T 100.0 100.0 100.0 100.0	96.2 NS/COMMENTS URING OCTOBER HE INSTALLAT 99.9 99.9 99.9 99.9	100.0 R MODULES E A ION OF BRACIN 100.0 100.0 100.0	95.0 ND A WERE OF G. 99.9 99.9 99.9 94.0	F-LINE	PART			FOR	88.0 95.3
11/81	** PROS	100.0 BLEMS/SOLUTIO T 100.0 100.0 100.0 100.0	96.2 NS/COMMENTS URING OCTOBER HE INSTALLAT: 99.9 99.9 99.9 94.0 .0 98.4	100.0 R MODULES E A ION OF BRACIN 100.0 100.0 100.0 100.0	95.0 ND A WERE OF G. 99.9 99.9 99.9 94.0 .0	F-LINE	PART	OF THE	E TIME P	FOR	
11/81	** PROS	100.0 BLEMS/SOLUTIO T 100.0 100.0 100.0 100.0 100.0 BLEMS/SOLUTIO	96.2 NS/COMMENTS URING OCTOBER HE INSTALLAT 99.9 99.9 94.0 .0 98.4 NS/COMMENTS URING NOVEMB	100.0 R MODULES E A ION OF BRACIN 100.0 100.0 100.0 100.0	95.0 ND A WERE OF G. 99.9 99.9 94.0 .0 98.0 NAS DOWN FOR	MAINTE	NANCE	OF THE	E TIME P	FOR 708	95.3
	** PROS	100.0 BLEMS/SOLUTIO T 100.0 100.0 100.0 100.0 100.0 BLEMS/SOLUTIO	96.2 NS/COMMENTS URING OCTOBER HE INSTALLAT 99.9 99.9 94.0 .0 98.4 NS/COMMENTS URING NOVEMB	100.0 R MODULES E A ION OF BRACIN 100.0 100.0 100.0 100.0	95.0 ND A WERE OF G. 99.9 99.9 94.0 .0 98.0 MAS DOWN FOR RROSION OF T	MAINTE	NANCE	OF THE	E TIME P	FOR 708	95.3
	** PROS	100.0 BLEMS/SOLUTIO T 100.0 100.0 100.0 100.0 20 100.0 BLEMS/SOLUTIO Q	96.2 NS/COMMENTS URING OCTOBER HE INSTALLAT 99.9 99.9 94.0 .0 98.4 NS/COMMENTS URING NOVEMB UENCHER SECT	100.0 R MODULES E A ION OF BRACIN 100.0 100.0 100.0 100.0 100.0 100.0 100.0	95.0 ND A WERE OF G. 99.9 99.9 94.0 .0 98.0 NAS DOWN FOR RROSION OF T	MAINTE	NANCE	OF THE	E TIME P	FOR 708	95.3
11/81	** PROS	100.0 BLEMS/SOLUTIO T 100.0 100.0 100.0 .0 100.0 BLEMS/SOLUTIO Q	96.2 NS/COMMENTS URING OCTOBER HE INSTALLAT 99.9 99.9 94.0 .0 98.4 NS/COMMENTS URING NOVEMB UENCHER SECT	100.0 R MODULES E A ION OF BRACIN 100.0 100.0 100.0 100.0	95.0 ND A WERE OF G. 99.9 99.9 94.0 .0 98.0 MAS DOWN FOR RROSION OF T	MAINTE	NANCE	OF THE	E TIME P	FOR 708	95.3

BASIN ELECTRIC POWER: LARAMIE RIVER 2 (CONT.)

_	MODULE A	VAILABILI	TY OPERABILITY			% RE		PER			CAP.
	E	100.0	65.6 92.6	100.0	52.9						
	SYSTEM	100.0	92.6	100.0	74.8			744	601	556	69.4
	** PROBL	EMS/SOLUT	IONS/COMMENTS								
			OUTAGE TIME DO THE ABSORBER WHICH ALSO AC	FEED TANK. G	ENERAL MAINT	ENANC	E WAS	PERFOR			
1/82	A	100.0		100.0	96.3						
	В		99.5	100.0							
	C	100.0	99.1	100.0	96.1						
	D	.0 100.0	.0	100.0	.0						
	E System	100.0	.0 94.7 98.1	100.0	91.8 95.0			744	722	708	93.3
			IONS/COMMENTS	20000	,510				,	, , ,	7505
	** PRODL	E1137 30 LUT		V THE MODINE	D 40000050		A187 114				
			DURING JANUAR			· EEU I	ANK WA	5 RESEA	ALED.		
2/82	A	100.0			94.7						
	В	100.0	87.6 75.7	100.0	83.1						
	C	100.0									
	D E	42.9 100.0		100.0 100.0	28.1						
	SYSTEM		96.0		84.6 91.0			672	638	609	83.9
	** PROBL	EMS/SOLUT	IONS/COMMENTS								
			THE SEAL COAT	ING OF THE D	ABSORBER FEE	D TAN	K CONT	INUED :	INTO FEI	BRUARY	•
			THE D MODULE PROTECTION.	WAS DOWN PART	OF THE TIME	то м	AKE RE	PAIRS '	TO THE	РОТЕНТ	IAL
3/82	A	48.4	33.8 69.4	100.0 100.0	31.5 64.8						
	В	70.7		100.0							
		100.0	69.4	100.0	64.8						
	C		69.4 84.2		64.8 78.6						
		100.0	84.2 93.0	100.0 100.0	64.8 78.6 86.8						
	С	100.0 100.0	84.2 93.0	100.0 100.0	78.6 86.8						
	C D	100.0 100.0 100.0 100.0	84.2 93.0	100.0 100.0 100.0	78.6 86.8			744	694	616	70.2
	C D E SYSTEM	100.0 100.0 100.0 100.0	84.2 93.0 74.4	100.0 100.0 100.0	78.6 86.8 69.4			744	694	616	70.2
	C D E SYSTEM	100.0 100.0 100.0 100.0	84.2 93.0 74.4 89.0	100.0 100.0 100.0 100.0	78.6 86.8 69.4 83.0	PROXIM	ATELY				
	C D E SYSTEM ** PROBL	100.0 100.0 100.0 100.0	84.2 93.0 74.4 89.0 IONS/COMMENTS	100.0 100.0 100.0 100.0	78.6 86.8 69.4 83.0	PROXIM	ATELY				
	C D E SYSTEM ** PROBL	100.0 100.0 100.0 100.0 100.0	84.2 93.0 74.4 89.0 IONS/COMMENTS DURING MARCH ABSORBER FEED	100.0 100.0 100.0 100.0	78.6 86.8 69.4 83.0 OFF-LINE APF	PROXIM	ATELY				
	C D E SYSTEM ** PROBL	100.0 100.0 100.0 100.0 100.0 EMS/SOLUT	84.2 93.0 74.4 89.0 IONS/COMMENTS DURING MARCH ABSORBER FEED	100.0 100.0 100.0 100.0 MODULE A WAS	78.6 86.8 69.4 83.0 OFF-LINE APP	PROXIM	ATELY				
	C D E SYSTEM ** PROBL	100.0 100.0 100.0 100.0 100.0 EMS/SOLUT	84.2 93.0 74.4 89.0 IONS/COMMENTS DURING MARCH ABSORBER FEED .0 33.3	100.0 100.0 100.0 100.0 MODULE A WAS TANK.	78.6 86.8 69.4 83.0 OFF-LINE APP	PROXIM	ATELY				
	C D E SYSTEM ** PROBL	100.0 100.0 100.0 100.0 100.0 EMS/SOLUT	84.2 93.0 74.4 89.0 IONS/COMMENTS DURING MARCH ABSORBER FEED .0 33.3 48.1 100.0 77.8	100.0 100.0 100.0 100.0 MODULE A WAS TANK. 100.0 100.0 100.0	78.6 86.8 69.4 83.0 OFF-LINE APF .0 1.2 1.8 3.8 2.9	PROXIM	ATELY	384 HO	JRS TO I	RESEAL	ТНЕ
	C D E SYSTEM ** PROBL	100.0 100.0 100.0 100.0 100.0 EMS/SOLUT	84.2 93.0 74.4 89.0 IONS/COMMENTS DURING MARCH ABSORBER FEED .0 33.3 48.1 100.0	100.0 100.0 100.0 100.0 MODULE A WAS TANK.	78.6 86.8 69.4 83.0 OFF-LINE APP .0 1.2 1.8 3.8	PROXIM	ATELY		JRS TO I		THE
	C D E SYSTEM ** PROBL A B C D E SYSTEM	100.0 100.0 100.0 100.0 100.0 EMS/SOLUT 6.7 26.7 3.3 23.3 26.7 21.7	84.2 93.0 74.4 89.0 IONS/COMMENTS DURING MARCH ABSORBER FEED .0 33.3 48.1 100.0 77.8	100.0 100.0 100.0 100.0 MODULE A WAS TANK. 100.0 100.0 100.0	78.6 86.8 69.4 83.0 OFF-LINE APF .0 1.2 1.8 3.8 2.9	PROXIM	ATELY	384 HO	JRS TO I	RESEAL	ТНЕ
4/82	C D E SYSTEM ** PROBL A B C D E SYSTEM	100.0 100.0 100.0 100.0 100.0 EMS/SOLUT 6.7 26.7 3.3 23.3 26.7 21.7	84.2 93.0 74.4 89.0 IONS/COMMENTS DURING MARCH ABSORBER FEED .0 33.3 48.1 100.0 77.8 64.8	100.0 100.0 100.0 100.0 MODULE A WAS TANK. 100.0 100.0 100.0	78.6 86.8 69.4 83.0 OFF-LINE APP .0 1.2 1.8 3.8 2.9 2.4			384 HOU 720	URS TO 1	RESEAL 18	THE
	C D E SYSTEM ** PROBL A B C D E SYSTEM	100.0 100.0 100.0 100.0 100.0 EMS/SOLUT 6.7 26.7 3.3 23.3 26.7 21.7	84.2 93.0 74.4 89.0 IONS/COMMENTS DURING MARCH ABSORBER FEED .0 33.3 48.1 100.0 77.8 64.8 IONS/COMMENTS	100.0 100.0 100.0 100.0 MODULE A WAS TANK. 100.0 100.0 100.0 100.0	78.6 86.8 69.4 83.0 OFF-LINE APP .0 1.2 1.8 3.8 2.9 2.4) SEAL	. COAT	720	URS TO 1 27 SORBER	18 FEED T	THE 1.3
	C D E SYSTEM ** PROBL A B C D E SYSTEM ** PROBL	100.0 100.0 100.0 100.0 100.0 EMS/SOLUT 6.7 26.7 3.3 23.3 26.7 21.7	84.2 93.0 74.4 89.0 IONS/COMMENTS DURING MARCH ABSORBER FEED .0 33.3 48.1 100.0 77.8 64.8 IONS/COMMENTS THE MODULES W MAINTENANCE W	100.0 100.0 100.0 100.0 MODULE A WAS TANK. 100.0 100.0 100.0 100.0	78.6 86.8 69.4 83.0 OFF-LINE APP .0 1.2 1.8 3.8 2.9 2.4) SEAL	. COAT	720	URS TO 1 27 SORBER	18 FEED T	THE 1.3

BASIN ELECTRIC POWER: LARAMIE RIVER 2 (CONT.)

PERIOD	MODULE		OPERABILITY	RELIABILIT	ANCE DATA Y UTILIZATION	% RE SO2	MOVAL PART.	PER			
	D	100.0	80.2								
	Ε	100.0	92.6	100.0	86.8						
	SYSTEM	98.4	76.2	100.0	71.5			744	697	532	75.6
	** PROE	BLEMS/SOLUTIO	NS/COMMENTS								
		ום	URING MAY MOD	ULE C WAS	TAKEN OFF-LINE	FOR I	MAINTE	NANCE A	ND REP	AIRS.	
6/82	A	100.0	89.3	100.0	89.3						
	В	86.7	69 .3	100.0	69.3						
	С	16.7	11.7	100.0	11.7						
	ם	100.0	76.1	100.0	76.1						
	E	100.0	96.9	100.0	96.9						
	SYSTEM	100.0	85.8	100.0	85.8			72 0	720	618	66.4
	** PROE	BLEMS/SOLUTION	NS/COMMENTS								
			URING JUNE MO		OUT OF SERVICE	E PAR	T OF TH	HE TIME	FOR NO	DZZLE R	REPAIR
7/82	A		54.7	100.0	43.6						
	В	61.3	55.2	100.0	44.1						
	C	100.0	77.8	100.0	62.1						
	D	100.0	91.0 45.9	100.0	72.7						
	E	74.2		100.0	36.7						
	SYSTEM	100.0	81.2	100.0	64.8			744	594	482	60.4
	** PROB	BLEMS/SOLUTION	NS/COMMENTS								
			URING JULY MO ECTION.	DULES A, B	AND E WERE DO	OT NW	REPAIR	NOZZL	ES IN 1	THE QUE	NCHER
8/82	A	80.6	67.0	100.0	63.9						
	В	100.0	93.9	100.0	89.5						
	С	100.0	97.4	100.0	92.8						
	D	22.6		100.0	20.6						
	Ε	83.9	21.7 58.0	100.0 100.0	55.2						
	SYSTEM				80.5			744	709	599	65.4
	** PROB	LEMS/SOLUTION	NS/COMMENTS								
		DU	JRING AUGUST	MODULES A	AND D WERE DOWN	Y FOR	MAINTE	NANCE	IN THE	QUENCH	ER
		51	ECITON RESULT	ING FROM CO	ORROSION OF THE	E UDD!	EHOLM 9	04L.			
9/82	A	100.0	98.7	100.0	94.3						
	В	100.0	99.9	100.0	95.4						
	С	36.7	38. 0	100.0	36.4						
	D	63.3	61.3	100.0	58.6						
	Ε	. 0	.0		.0						
	SYSTEM	75.0	74.5	100.0	71.2			720	688	513	46.0
	** PROB	LEMS/SOLUTION	15/COMMENTS								
		D.C Q.C	RING SEPTEMB JENCHER SECTION	ER MODULES ON RESULTIN	C, D AND E WER	RE DON	IN FOR	MAINTE DDEHOL	NANCE I M 904L.	N THE	
10/82		25.8	24.5	100.0	24.4						
	В	39.7	34.2	100.0	34.0						
	С	77.4	72.5	100.0	72.2						
	D	74.2	72.7	100.0	72.4						
	Ε	100.0	98.9	100.0	98.5						
	SYSTEM	79.0	75.7	100.0	75.4			744	741	561	41.8

		PERFORMAN	NCE DATA	 	 	
PERIOD MODULE AVAILABILITY						
PERIOD HODOLE AVAILABILITY	OFERABLETT	KELIADILIII	OTTLIZATION			FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

DURING OCTOBER MODULE A WAS DOWN FOR MAINTENANCE ON WELDS IN THE QUENCHER SECTION RESULTING FROM CORROSION OF THE UDDEHOLM 904L.

DURING OCTOBER MODULE D WAS DOWN FOR REPAIRS OF BRACING.

11/82	A	.0	.0		.0				
	В	63.3	33.1	100.0	22.8				
	С	100.0	97.9	100.0	67.3				
	D	100.0	63.4	100.0	43.6				
	E	100.0	93.6	100.0	64.3				
	SYSTEM	90.8	72. 0	100.0	49.5	720	495	356	41.0

** PROBLEMS/SOLUTIONS/COMMENTS

DURING NOVEMBER MODULES A AND B WERE DOWN FOR MAINTENANCE ON WELDS IN THE QUENCHER SECTION RESULTING FROM CORROSION OF THE UDDEHOLM 904L.

12/82	A	32.3	27.1	100.0	26.2				
	В	100.0	90.4	100.0	87.3				
	С	100.0	97.2	100.0	93.9				
	D	100.0	50.2	100.0	48.6				
	E	100.0	100.0	100.0	96.6				
	SYSTEM	100.0	91.2	100.0	88.2	744	719	656	68.8

** PROBLEMS/SOLUTIONS/COMMENTS

DURING DECEMBER MODULE A WAS DOWN FOR MAINTENANCE ON THE TOWER MIXERS AND WETTED FILM CONTACT PACKING.

1/83	A	100.0	92.2	100.0	71.6				
	В	22.6	9.4	100.0	7.3				
	С	100.0	88.1	100.0	68.4				
	D	83.9	74.2	100.0	57.7				
	E	100.0	81.2	100.0	63.1				
	SYSTEM	100.0	86.3	100.0	67.0	744	578	498	61.1

** PROBLEMS/SOLUTIONS/COMMENTS

DURING JANUARY MODULE B WAS DOWN TO ROUND OFF WELDS IN THE SCRUBBER.

2/83	A	25.0	16.5	100.0	15.1				
	В	89.3	72.9	100.0	66.7				
	С	100.0	96.6	100.0	88.4				
	D	100.0	57.8	100.0	52.9				
	E	85.7	72.3	100.0	66.2				
	SYSTEM	100.0	79.0	100.0	72.3	672	615	486	53.1

** PROBLEMS/SOLUTIONS/COMMENTS

DURING FEBRUARY MODULE A WAS DOWN DUE TO PROBLEMS WITH THE INLET ISOLATION GUILLOTINE DAMPER.

DURING FEBRUARY MODULE E WAS DOWN TO CLEAN THE TOWER PACKING.

3/83	A	100.0	95.4	100.0	90.3			
	В	100.0	83.7	100.0	79.2			
	С	100.0	93.9	100.0	88.8			
	D	100.0	46.6	100.0	44.1			
	Ε	51.6	28.8	100.0	27.2			
	SYSTEM	100.0	87.1	100.0	82.4	744	704	613 62.4

BASIN ELECTRIC POWER: LARAMIE RIVER 2 (CONT.)

4/83 A B C D E SY *** 6/83 A B C D E SY *** 7/83 A B C D E SY ***	YSTEM * PROBI YSTEM * PROBI	99.9 99.9 46.7 99.9 100.0 LEMS/SOLUT	74.1 45.1 31.5 96.4 86.5 TONS/COMMENTS MODULE C WAS AND GENERAL T 95.4 92.1 .0 92.3 75.4 88.8 TONS/COMMENTS MODULE C WAS 100.0 76.5 8.0 85.6	100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0	98.6 73.9 45.0 31.5 96.1 86.3 APRIL FOR A C ANCE. 56.5 54.6 .0 54.7 44.7 52.6	LEANING OF	720 THE ABS	718 ORBER P 441	621 ACKING 392	64.0
5/83 A B C D E SY ** 6/83 A B C D E SY **	YSTEM * PROBI YSTEM * PROBI	99.9 46.7 99.9 99.9 100.0 LEMS/SOLUT 100.0 100.0 100.0 100.0 100.0 100.0 100.0	70 CLEAN THE 98.9 74.1 45.1 31.5 96.4 86.5 FIONS/COMMENTS MODULE C WAS AND GENERAL T 95.4 92.1 .0 92.3 75.4 88.8 FIONS/COMMENTS MODULE C WAS 100.0 76.5 8.0 85.6	100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0	98.6 73.9 45.0 31.5 96.1 86.3 APRIL FOR A C ANCE. 56.5 54.6 .0 54.7 44.7 52.6	LEANING OF	720 THE ABS	718 ORBER P 441	621 ACKING 392	64.0
5/83 A B C D E SY ** 6/83 A B C D E SY **	YSTEM * PROBI YSTEM * PROBI	99.9 46.7 99.9 99.9 100.0 LEMS/SOLUT 100.0 100.0 100.0 100.0 100.0 100.0 100.0	74.1 45.1 31.5 96.4 86.5 IONS/COMMENTS MODULE C WAS AND GENERAL T 95.4 92.1 .0 92.3 75.4 88.8 IONS/COMMENTS MODULE C WAS 100.0 76.5 8.0 85.6	100.0 100.0 100.0 100.0 100.0 100.0 DOWN DURING A 100.0 100.0 100.0 100.0 100.0	73.9 45.0 31.5 96.1 86.3 APRIL FOR A C ANCE. 56.5 54.6 .0 54.7 44.7 52.6 MAY FOR MAINT 100.0 76.5 8.0		THE ABS	ORBER P	ACKING 392	64.7
5/83 A B C D E SY *** 7/83 A B C D E SY ***	YSTEM * PROBI	46.7 99.9 99.9 100.0 LEMS/SOLUT 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0	45.1 31.5 96.4 86.5 TIONS/COMMENTS MODULE C WAS AND GENERAL T 95.4 92.1 .0 92.3 75.4 88.8 TIONS/COMMENTS MODULE C WAS 100.0 76.5 8.0 85.6	100.0 100.0 100.0 100.0 100.0 DOWN DURING A 100.0 100.0 100.0	45.0 31.5 96.1 86.3 APRIL FOR A C ANCE. 56.5 54.6 .0 54.7 44.7 52.6 MAY FOR MAINT 100.0 76.5 A 0		THE ABS	ORBER P	ACKING 392	64.7
5/83 A B C D E SY *** 6/83 A B C D E SY ***	YSTEM * PROBI YSTEM * PROBI	99.9 99.9 100.0 LEMS/SOLUT 100.0 100.0 100.0 100.0 100.0 100.0 100.0	96.4 86.5 TIONS/COMMENTS MODULE C WAS AND GENERAL T 95.4 92.1 .0 92.3 75.4 88.8 TIONS/COMMENTS MODULE C WAS 100.0 76.5 8.0 85.6	100.0 100.0 DOWN DURING / OWER MAINTEN/ 100.0 100.0 100.0 100.0	96.1 86.3 APRIL FOR A C ANCE. 56.5 54.6 .0 54.7 44.7 52.6 MAY FOR MAINT 100.0 76.5 8.0		THE ABS	ORBER P	ACKING 392	64.7
5/83 A B C D E SY *** 6/83 A B C D E SY ***	YSTEM * PROBI YSTEM * PROBI	99.9 100.0 LEMS/SOLUT 100.0 100.0 100.0 100.0 LEMS/SOLUT 100.0 13.3 100.0	96.4 86.5 TIONS/COMMENTS MODULE C WAS AND GENERAL T 95.4 92.1 .0 92.3 75.4 88.8 TIONS/COMMENTS MODULE C WAS 100.0 76.5 8.0 85.6	100.0 100.0 DOWN DURING / OWER MAINTEN/ 100.0 100.0 100.0 100.0	96.1 86.3 APRIL FOR A C ANCE. 56.5 54.6 .0 54.7 44.7 52.6 MAY FOR MAINT 100.0 76.5 8.0		THE ABS	ORBER P	ACKING 392	64.7
5/83 A B C D E SY *** 6/83 A B C D E SY ***	YSTEM * PROBI YSTEM * PROBI	100.0 LEMS/SOLUT 100.0 100.0 100.0 100.0 100.0 100.0 1.00.0 1.00.0 1.00.0 1.00.0	86.5 IONS/COMMENTS MODULE C WAS AND GENERAL T 95.4 92.1 .0 92.3 75.4 88.8 IONS/COMMENTS MODULE C WAS 100.0 76.5 8.0 85.6	100.0 DOWN DURING A TOWER MAINTENA 100.0 100.0 100.0 100.0 100.0	86.3 APRIL FOR A C ANCE. 56.5 54.6 .0 54.7 44.7 52.6 MAY FOR MAINT 100.0 76.5 A 0		THE ABS	ORBER P	ACKING 392	64.7
5/83 A B C D E SY *** 6/83 A B C D E SY ***	YSTEM * PROBI	100.0 100.0 .0 100.0 100.0 100.0 .EMS/SOLUT	MODULE C WAS AND GENERAL T 95.4 92.1 .0 92.3 75.4 88.8 TONS/COMMENTS MODULE C WAS 100.0 76.5 8.0 85.6	100.0 100.0 100.0 100.0 100.0 100.0	56.5 54.6 .0 54.7 44.7 52.6 MAY FOR MAINT 100.0 76.5 8.0		744	441	392	64.7
6/83 A B C D E SY ***	YSTEM * PROBI	100.0 .0 100.0 100.0 100.0 LEMS/SOLUT	AND GENERAL T 95.4 92.1 .0 92.3 75.4 88.8 TONS/COMMENTS MODULE C WAS 100.0 76.5 8.0 85.6	100.0 100.0 100.0 100.0 100.0 100.0	56.5 54.6 .0 54.7 44.7 52.6 MAY FOR MAINT 100.0 76.5 8.0		744	441	392	64.7
6/83 A B C D E SY ***	YSTEM * PROBI	100.0 .0 100.0 100.0 100.0 LEMS/SOLUT	92.1 .0 92.3 75.4 88.8 TIONS/COMMENTS MODULE C WAS 100.0 76.5 8.0 85.6	100.0 100.0 100.0 100.0 DOWN DURING 1	54.6 .0 54.7 44.7 52.6 MAY FOR MAINT 100.0 76.5 8.0	ENANCE IN T				
6/83 A B C D E SY ***	YSTEM * PROBI	100.0 .0 100.0 100.0 100.0 LEMS/SOLUT	92.1 .0 92.3 75.4 88.8 TIONS/COMMENTS MODULE C WAS 100.0 76.5 8.0 85.6	100.0 100.0 100.0 100.0 DOWN DURING 1	54.6 .0 54.7 44.7 52.6 MAY FOR MAINT 100.0 76.5 8.0	ENANCE IN T				
6/83 A B C D E SY ***	YSTEM * PROBI	100.0 100.0 100.0 LEMS/SOLUT 100.0 100.0 13.3 100.0	92.3 75.4 88.8 TIONS/COMMENTS MODULE C WAS 100.0 76.5 8.0 85.6	100.0 100.0 100.0 DOWN DURING 1	.0 54.7 44.7 52.6 MAY FOR MAINT 100.0 76.5	ENANCE IN T				
6/83 A B C D E SY ***	YSTEM * PROBI	100.0 LEMS/SOLUT 100.0 100.0 13.3 100.0	88.8 IONS/COMMENTS MODULE C WAS 100.0 76.5 8.0 85.6	100.0 DOWN DURING 1 100.0 100.0	52.6 MAY FOR MAINT 100.0 76.5 8.0	ENANCE IN T				
6/83 A B C D E SY ***	YSTEM * PROBI	100.0 LEMS/SOLUT 100.0 100.0 13.3 100.0	88.8 IONS/COMMENTS MODULE C WAS 100.0 76.5 8.0 85.6	100.0 DOWN DURING 1 100.0 100.0	52.6 MAY FOR MAINT 100.0 76.5 8.0	ENANCE IN T				
6/83 A B C D E SY		100.0 100.0 100.0 13.3 100.0	IONS/COMMENTS MODULE C WAS 100.0 76.5 8.0 85.6	DOWN DURING 1 100.0 100.0	100.0 100.5 8.0	ENANCE IN T	THE QUEN	CHER SE	CTION.	
7/83 A B C D E SY		100.0 13.3 100.0	100.0 76.5 8.0 85.6	100.0 100.0	100.0 76.5	ENANCE IN T	тне фиек	CHER SE	CTION.	
7/83 A B C D E SY		100.0 13.3 100.0	8.0 85.6	100.0	76.5 A 0					
7/83 A B C D E SY		13.3	8.0 85.6	100.0	76.5 A 0					
7/83 A B C D E SY		100.0	8.0 85.6	100.0	A 0					
7/83 A B C D E SY		100.0	05.6	700 0	0.0					
7/83 A B C D E SY				100.0	85.6 81.3					
7/83 A B C D E SY		100.0	87.9	100.0 100.0	87.9		720	720	633	65.0
B C D E SY	* PROBI	EMS/SOLUT	IONS/COMMENTS							
B C D E SY			MODULE C WAS	DOWN DURING .	JUNE FOR MAIN	TENANCE.				
C D E SY		48.1			41.4					
D E SY			84.0		79.1					
E SY		100.0	98.1		92.4					
SY		100.0 64.5	83.2 33.8	100. 0 100.0						
××	YSTEM	100.0	85.8	100.0	31.8 80.8		744	701	601	57.6
	× PROBι	EMS/SOLUT	IONS/COMMENTS							
			MODULES A AND SECTION.	E WERE DOWN	DURING PART	OF JULY FOR	REPAIR	S IN TH	E QUEN	CHER
8/83 A		35.5	31.4	100.0	30.9					
В		71.0	66.6	100.0	65.7					
C		100.0	95.0	100.0	93.6					
D E		100.0	99.1	100.0	97.6					
	YSTEM	100.0 100.0	60.4 88.1	100.0 100.0	59.5 86.8		744	733	646	62.7
**			IONS/COMMENTS				, , , ,	, ,,	040	02.7
~~	e ppne:	FMS/SOLIT	TOMOS COMMENTS							

9/83 A 100.0 64.0 100.0 3.8

PERIOD	MODULE	AVAILABILITY			NCE DATA UTILIZATION	% RE	MOVAL	PER	BOILER		CAP. FACTOR
	В	26.7	.0		.0				•		
	С	100.0	98.8	100.0	5.9						
	D	73.3	100.0	100.0	6.0						
	Ε	100.0	99.4	100.0	5.9						
	SYSTEM	100.0	90.6	100.0	5.4			720	43	39	59.7
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			ODULES B AND UENCHER TOWE	_	DURING PART	OF SE	PTEMBE	R FOR 1	1AINTEN	ANCE O	THE
10/83	A	100.1	92.7	100.0	16.3 16.5						
	В	100.1	93.9	100.0							
	C	100.1	100.0	100.0							
	D	.0	.0		.0						
	E	100.1	80.5	100.0	14.2						
	SYSTEM	100.0	91.8	100.0	16.2			744	131	121	72.2
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			ODULE D WAS UENCHER SECT		PART OF OCTOR	BER FO	R MAIN	TENANCI	E ON WE	LDS IN	THE
		A	BSORBER RECY	CLE TANK MIX	ERS WERE REPA	IRED	AT MOD	ULE D I	OURING	THE MOI	NTH.
11/83	A	100.0			.0						
	В	100.0			.0						
	C	100.0			.0						
	D E	43.3 46.7			. 0 . 0						
	SYSTEM				.0			720	0	0	.0
12/83	A	100.0	93.3	100.0	28.0						
	В	100.0	98.7	100.0	28.0 29.6						
	С	100.0	91.0	100.0	27.3						
	D	100.0	. 0		.0						
	E	41.9	0		.0						
	SYSTEM	100.0	70.7	100.0	21.2			744	223	158	42.4
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			HE UNIT WAS OW POWER DEM		IRE MONTH OF	NOVEM	BER AN	D MOST	OF DEC	EMBER 1	DUE TO
1/84	A	100.0	99.3	100.0	55.2						
	В	100.0	95.5	100.0	53.1						
	C	100.0	97.7	100.0	54.4						
	D	100.0	. 0		.0						
	E System	100.0 100.0	.0 73.1	100.0	.0 40.7			744	414	303	42.9
2/84	A	100.0			.0						
	В	100.0			.0						
	С	100.0			.0						
	D	100.0			.0						
	Ε	100.0			. 0						
	SYSTEM	100.0			.0			696	0	0	.0
3/84	A	100.0			.0						
	В	100.0			.0						
	C	100.0			.0						
	D	100.0			.0						
	E	100.0 100.0			.0			744	^	_	^
	SYSTEM	100.0			. U			/44	0	0	.0

BASIN ELECTRIC POWER: LARAMIE RIVER 2 (CONT.)

ERIOD	MODULE	AVAILABILI	TY OPERABILITY	RELIABILITY	UTILIZATION	% REMOV	VAL	PER	BOILER	FGD HOURS	CAP.
	** PROE	SLEMS/SOLUT	IONS/COMMENTS								
			THE UTILITY RIDURING THE FI			-RELATE) PRC	BLEMS	WERE E	NCOUNTE	ERED
4/84	A	.0			.0						
	В	.0			.0						
	С	.0			.0						
	D	.0			.0						
	Ε	.0			.0						
	SYSTEM	.0			.0			720	0	0	.0
	** PROB	BLEMS/SOLUT	IONS/COMMENTS								
			A UNIT OUTAGE	OCCURRED DU	RING THE MONT	TH OF API	RIL.				
5/84		6.5			.0						
	В	9.7			.0						
	C	.0			.0						
	D	3.2			.0						
	E	9.7			.0			7//	•	•	
	SYSTEM	7.3			.0			/44	0	0	.0
	** PRO	BLEMS/SOLUT	IONS/COMMENTS								
			THE UTILITY R		THE UNIT WAS	DOWN FO	OR MA	INTEN	ANCE ON	ALL	
6/84	A	100.0	84.6	100.0	72.6						
	В	100.0		100.0	78.7						
	С	33.3	35.2	100.0	30.2						
	D	93.3	63.2	100.0	54.2						
	Ε	100.0	95.4	100.0	81.9						
	SYSTEM				79.4			720	618	572	77.0
	** PRO	BLEMS/SOLUT	IONS/COMMENTS								
			MODULE C WAS	DOWN FOR MED	HANICAL REPAI	RS DURI	NG JU	NE.			
7/84	A	100.0	44.2	100.0	44.2						
	В	100.0	85.7	100.0	85.7						
	С	67.7	64.4	100.0	64.4						
	D	90.3	72.8	100.0	72.8						
	E	100.0	94.2	100.0	94.2						
	SYSTEM	100.0	90.3	100.0	90.3			744	744	672	75.4
	** PRO	BLEMS/SOLUT	IONS/COMMENTS								
			THE UTILITY R	EPORTED THAT	NO MAJOR FGE	-RELATE	D PRO	BLEMS	AROSE	DURING	JULY.
	A	100.0	76.8	100.0	76.5						
8/84	_	100.0	89.3	100.0	89.0						
8/84	В										
8/84	C	29.0	8.4	100.0	8.3						
8/84		29.0 100.0	8.4 92.0	100.0 10 0. 0	8.3 91.6						
8/84	С										

** PROBLEMS/SOLUTIONS/COMMENTS

MODULE C WAS DOWN DURING PART OF AUGUST FOR ABSORBER MIXER REPAIRS.

WELDING WAS DONE IN THE QUENCHER SECTION DURING AUGUST.

9/84 SYSTEM 720

BASIN ELECTRIC POWER: LARAMIE RIVER 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR SEPTEMBER 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COMPANY NAME PLANT NAME UNIT NUMBER CITY STATE REGULATORY CLASSIFICATION	BASIN ELECTRIC LARAMIE RIVER 3 WHEATLAND WYOMING A	POWER
PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW NET UNIT GENERATING CAPACITY W/FGD - MW NET UNIT GENERATING CAPACITY W/FGD - MW EQUIVALENT SCRUBBED CAPACITY - MW	43. 86.	(.100 LB/MMBTU) (.200 LB/MMBTU) (****** LB/MMBTU)
** UNIT DATA - BOILER AND STACK BOILER SUPPLIER	BABCOCK & WILCO	ox
BOILER TYPE	PULVERIZED COAL	-
BOILER SERVICE LOAD DESIGN BOILER FLUE GAS FLOW - CU.M/S BOILER FLUE GAS TEMPERATURE - C STACK HEIGHT - M STACK SHELL	69.4	(2800000 ACFM) (157 F) (600 FT)
STACK TOP DIAMETER - M	8.7	(28.6 FT)
** FUEL DATA	6041	
FUEL TYPE FUEL GRADE	COAL SUBBITUMINOUS	
AVERAGE HEAT CONTENT J/G		(8400 BTU/LB)
RANGE HEAT CONTENT BTU/LB		7906-8244
AVERAGE ASH CONTENT - %	7.89	
RANGE ASH CONTENT // AVERAGE MOISTURE CONTENT - //	4.0-13.0 28.92	
RANGE MOISTURE CONTENT - %	22.2-34.7	
AVERAGE SULFUR CONTENT - %	.54	
RANGE SULFUR CONTENT // AVERAGE CHLORIDE CONTENT - //	0.2-0.5	
RANGE CHLORIDE CONTENT - %	.04 0.00-0.04	
*** PARTICLE CONTROL	• • • • • • • • • • • • • • • • • • • •	
** FABRIC FILTER		
NUMBER	0	
TYPE	NONE	
** ESP		
NUMBER	1	
TYPE	COLD SIDE	
SUPPLIER	BABCOCK & WILCO	
INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE - C	1085.4	(2300000 ACFM)
PRESSURE DROP - KPA	69.4 .2	(157 F) (1. IN-H20)
PARTICLE REMOVAL EFFICENCY - %	99.6	21 211 1120
XX DARTICLE CONTROLS		
** PARTICLE SCRUBBER NUMBER	0	
GENERIC TYPE	NONE	
SPECIFIC TYPE	N/A	
TRADE NAME/COMMON NAME	N/A	
SHELL GENERIC MATERIAL SHELL SPECIFIC MATERIAL	N/A	
LINER GENERIC MATERIAL	N/A N/A	
LINER SPECIFIC MATERIAL	N/A	
GAS CONTACTING DEVICE TYPE	N/A	
*** FGD SYSTEM		

*** FGD SYSTEM

BASIN ELECTRIC POWER: LARAMIE RIVER 3 (CONT.)

** GENERAL DATA

```
SALEABLE PRODUCT/THROWAWAY PRODUCT
                                               THROWAWAY PRODUCT
   SO2 REMOVAL MODE
                                               SPRAY DRYING
   PROCESS TYPE
                                               LIME/SPRAY DRYING
   SYSTEM SUPPLIER
                                               BABCOCK & WILCOX
                                               BURNS & MCDONNELL
   A-E FIRM
   DEVELOPMENT LEVEL
                                                FULL SCALE
   NEW/RETROFIT
                                               NEW
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.60
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - X
                                                  82.50
   CURRENT STATUS
   COMMERCIAL START-UP
                                               11/82
   INITIAL START-UP
                                               11/82
   CONTRACT AWARDED
                                               10/78
** DESIGN AND OPERATING PARAMETERS
** QUENCHER/PRESATURATOR
   CONSTRUCTION MATERIAL GENERIC TYPE
                                               NR
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               NP
** ABSORBER
   NUMBER
                                                 4
   NUMBER OF SPARES
                                                SPRAY DRYER
   GENERIC TYPE
   SPECIFIC TYPE
                                                NR
   TRADE NAME/COMMON TYPE
                                               HYDRAULIC PRESSURE NOZZLE
   SUPPLIER
                                               BABCOCK & WILCOX
   DIMENSIONS - FT
                                                54'8"W X 46'10"H
   SHELL GENERIC MATERIAL
                                                CARBON STEEL
                                               AISI 1110
   SHELL SPECIFIC MATERIAL
   SHELL MATERIAL TRADE NAME/COMMON TYPE
                                                N/A
    LINER GENERIC MATERIAL
                                                NONE
    LINER SPECIFIC MATERIAL
                                                N/A
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                                N/A
    GAS CONTACTING DEVICE TYPE
                                                NONE
   NUMBER OF CONTACTING ZONES
                                                 2
                                                              ( 0 GPM)
( .3 GAL/1000 ACF)
    LIQUID RECIRCULATION RATE - LITER/S
                                                    0.
    L/G RATIO - L/CU.M
                                                    .0
    GAS-SIDE PRESSURE DROP - KPA
                                                    1.6
                                                               ( 6.5 IN-H20)
                                                               ( 5.0 FT/S)
    SUPERFICAL GAS VELOCITY - M/SEC
                                                    1.5
    INLET GAS FLOW - CU. M/S
                                                  377.52
                                                               ( 800000 ACFM)
   INLET GAS TEMPERATURE C
SO2 REMOVAL EFFICIENCY. %
                                                  137.2
                                                               ( 279 F)
                                                  85.0
   PARTICLE REMOVAL EFFICENCY - %
                                                   99.6
** MIST ELIMINATOR
   PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                                NONE
   GENERIC TYPE
                                                N/A
    SPECIFIC TYPE
                                                N/A
    TRADE NAME/COMMON TYPE
                                                N/A
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                NR
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                NR
** REHEATER
   GENERIC TYPE
                                                BYPASS
                                                COLD SIDE
   SPECIFIC TYPE
   TRADE NAME/COMMON TYPE
                                                N/A
                                                   3.0
   PERCENT GAS BYPASSED - AVG
   INLET FLUE GAS FLOW RATE - CU. M/S
                                                               ( 105800 ACFM)
                                                   49.93
   INLET FLUE GAS TEMPERATURE - C
                                                  371.1
                                                               ( 700 F)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                                NR
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                NR
** FANS
                                                NR
   DESIGN
   FUNCTION
                                                NA
                                                ΝR
   APPLICATION
   SERVICE
                                                DRY
   CONSTRUCTION MATERIAL GENERIC TYPE
                                                NA
```

BASIN ELECTRIC POWER: LARAMIE RIVER 3 (CONT.)

** DAMPERS

NUMBER 4
FUNCTION SHUT-OFF
GENERIC TYPE LOUVER

SPECIFIC TYPE PARALLEL BLADE MULTILOUVER

CONSTRUCTION MATERIAL GENERIC TYPE NR
CONSTRUCTION MATERIAL SPECIFIC TYPE NR
LINER GENERIC MATERIAL TYPE NR
LINER SPECIFIC MATERIAL TYPE NR

** DAMPERS

NUMBER 4
FUNCTION CONTROL
GENERIC TYPE LOUVER

SPECIFIC TYPE PARALLEL BLADE MULTILOUVER

** DUCTWORK

SHELL GENERIC MATERIAL TYPE

SHELL SPECIFIC MATERIAL TYPE

LINER GENERIC MATERIAL TYPE

LINER SPECIFIC MATERIAL TYPE

NR

NR

** REAGENT PREPARATION EQUIPMENT

FUNCTION WET BALL MILL
DEVICE COMPARTMENTED
DEVICE TYPE NR

DEVICE TYPE NR NUMBER 2

FULL LOAD DRY FEED CAPACITY - M.TONS/HR 5.4 (6 TPH)

PRODUCT QUALITY - % SOLIDS 30.0

** REAGENT PREPARATION EQUIPMENT

FUNCTION SLAKER
DEVICE NR
DEVICE TYPE NR
NUMBER 2

FULL LOAD DRY FEED CAPACITY - M.TONS/HR 5.4 (6 TPH)

** TANKS

SERVICE NUMBER
----ABSORBER RECYCLE ****
NR ****
REAGENT PREP PRODUCT ****

** PUMPS

 SERVICE
 NUMBER

 ---- ----

 NR

** SOLIDS CONCENTRATING/DEWATERING

DEVICE NONE

*** SLUDGE

** TREATMENT

METHOD N/A
DEVICE N/A
PROPRIETARY PROCESS N/A

** DISPOSAL

NATURE FINAL
TYPE LANDFILL
LOCATION ON-SITE
SITE TREATMENT NONE

** PROCESS CONTROL AND INSTRUMENTATION

CHEMICAL PARAMETERS SO2, ACFM, SOLIDS PROCESS CONTROL MANNER AUTOMATIC

BASIN ELECTRIC POWER: LARAMIE RIVER 3 (CONT.)

** WATER BALANCE

WATER LOOP TYPE OPEN

EVAPORATION WATER LOSS - LITER/S 22.9 (363 GPM)
MAKEUP WATER ADDITION - LITERS/S 4.6 (73 GPM)

** CHEMICALS AND CONSUMPTION

FUNCTION ABSORBENT NAME LIME CONSUMPTION 3 TPH

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS HOURS FACTOR

11/82 SYSTEM

720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT INITIAL START-UP OCCURRED DURING NOVEMBER 1982.

12/82	SYSTEM	744
1/83	SYSTEM	744
2/83	SYSTEM	672
3/83	SYSTEM	744
4/83	SYSTEM	720
5/83	SYSTEM	744
6/83	SYSTEM	720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE FGD SYSTEM IS CURRENTLY BEING TESTED AND IS STILL IN THE SHAKEDOWN/DEBUGGING PHASE OF OPERATION.

7/83	SYSTEM	744
8/83	SYSTEM	744
9/83	SYSTEM	720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY CONTINUED PERFORMANCE TESTING ON THE FGD SYSTEM DURING THE THIRD QUARTER OF 1983.

10/83	SYSTEM	744
11/83	SYSTEM	720
12/83	SYSTEM	744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT LARAMIE RIVER 3 DID NOT OPERATE DURING THE FOURTH QUARTER DUE TO MAJOR DESIGN MODIFICATIONS OF THE SPRAY DRYER AND SLURRY PREPARATION SECTIONS.

 1/84
 SYSTEM
 744

 2/84
 SYSTEM
 696

 3/84
 SYSTEM
 744

BASIN ELECTRIC POWER: LARAMIE RIVER 3 (CONT.)

			 PERFORMAN	CE DATA	 			
		AVAILABILITY						CAP.
							HOURS	FACTOR
	6V67514					700		
4/84	SYSTEM					720		
5/84	SYSTEM					744		
2,01	3137611							
6/84	SYSTEM					720		
7/84	SYSTEM					744		

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE FGD SYSTEM WAS DOWN DURING THE PERIOD OF JANUARY THROUGH JULY, 1984 DUE TO A CONTINUATION OF MAJOR DESIGN MODIFICATIONS IN THE SPRAY DRYER AND THE SLURRY PREPARATION SYSTEM.

 8/84
 SYSTEM
 744

 9/84
 SYSTEM
 720

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR AUGUST AND SEPTEMBER 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COMPANY NAME	BIG RIVERS ELEC	TRIC
	D.B. WILSON	71 -
PLANT NAME		
UNIT NUMBER	1	
CITY	CENTERTOWN	
STATE	KENTUCKY	
	A	
PARTICULATE EMISSION LIMITATION - NG/J		(**** LB/MMBTU)
SO2 EMISSION LIMITATION - NG/J	*****	(***** LB/MMBTU)
NOX EMISSION LIMITATION - NG/J	*****	(**** LB/MMBTU)
NET PLANT GENERATING CAPACITY - MW	880	
GROSS UNIT GENERATING CAPACITY - MW	880 440	
NET UNIT GENERATING CAPACITY W/FGD - MW	495	
NET UNIT GENERATING CAPACITY WO/FGD - MW	495	
EQUIVALENT SCRUBBED CAPACITY - MW	440	
WE INITE BATA DOTLED AND STACK		
** UNIT DATA + BOILER AND STACK		
BOILER SUPPLIER	FOSTER WHEELER	
BOILER TYPE	PULVERIZED COAL	
BOILER SERVICE LOAD	BASE	
	*****	(VXXXXXV IAFM)
DESIGN BUILER PLUE GAS PLUM - CU.II/S	****	(AXXXXX ACFII)
BOILER FLUE GAS TEMPERATURE - C	****** *****	(*** F)
STACK HEIGHT - M	*****	(*** FT)
STACK SHELL	NR	
STACK TOP DIAMETER - M	*****	(XXXXX ET)
STACK TOP DIAMETER - M	*****	(XXXXX [])
** FUEL DATA		
FUEL TYPE	COAL	
FUEL GRADE	BITUMINOUS	
	61101111003	/ www.www. martin m. t.
AVERAGE HEAT CONTENT - J/G	****	(***** BTU/LB)
RANGE HEAT CONTENT - BTU/LB		9600-11600
AVERAGE ASH CONTENT - %	*****	
RANGE ASH CONTENT - %	15.0-25.0	

	8.0-14.0	
AVERAGE SULFUR CONTENT - %	3.75	
RANGE SULFUR CONTENT %	2.5-5.0	

RANGE CHLORIDE CONTENT - %	*****	
*** PARTICLE CONTROL		
** ESP		
	•	
NUMBER	2	
TYPE	COLD SIDE	
SUPPLIER	BUELL DIVISION	, ENVIROTECH
INLET FLUE GAS CAPACITY - CU.M/S	412.9	(875000 ACFM)
INLET FLUE GAS TEMPERATURE - C		(325 F)
INLET FLUE GAS TEMPERATURE - C	162.6	(325 F)
** PARTICLE SCRUBBER		
NUMBER	0	
GENERIC TYPE	NONE	
SPECIFIC TYPE	N/A	
TRADE NAME/COMMON NAME	N/A	
SHELL GENERIC MATERIAL	N/A	
SHELL SPECIFIC MATERIAL	N/A	
LINER GENERIC MATERIAL	N/A	
LINER SPECIFIC MATERIAL	N/A	
GAS CONTACTING DEVICE TYPE	N/A	
*** FGD SYSTEM		
** GENERAL DATA		
	TUROLIALIAY DROP	LICT
SALEABLE FRODUCT/THROWAWAY PRODUCT	THROWAWAY PROD	001
SO2 REMOVAL MODE	WET SCRUBBING	
PROCESS TYPE	LIME	
SYSTEM SUPPLIER	M.W. KELLOGG	
A-E FIRM	BURNS & ROE	
DEVELOPMENT LEVEL	FULL SCALE	
NEW/RETROFIT	NEW	

BIG RIVERS ELECTRIC: D.B. WILSON 1 (CONT.)

CURRENT STATUS 1
COMMERCIAL START-UP 9/84
INITIAL START-UP 9/84
CONTRACT AWARDED 8/80

** DESIGN AND OPERATING PARAMETERS

** QUENCHER/PRESATURATOR

CONSTRUCTION MATERIAL GENERIC TYPE NR
CONSTRUCTION MATERIAL SPECIFIC TYPE NR

** ABSORBER

NUMBER 3
GENERIC TYPE SPRAY TOWER

SPECIFIC TYPE OPEN CROSSCURRENT SPRAY
TRADE NAME/COMMON TYPE HORIZONTAL SPRAY CHAMBER

SHELL GENERIC MATERIAL
SHELL SPECIFIC MATERIAL
SHELL SPECIFIC MATERIAL
SHELL MATERIAL TRADE NAME/COMMON TYPE
NR
LINER GENERIC MATERIAL
LINER SPECIFIC MATERIAL
LINER MATERIAL TRADE NAME/COMMON TYPE
NR
GAS CONTACTING DEVICE TYPE
NONE

** MIST ELIMINATOR

PRE-MIST ELIMINATOR/MIST ELIMINATOR

GENERIC TYPE

SPECIFIC TYPE

TRADE NAME/COMMON TYPE

CONSTRUCTION MATERIAL GENERIC TYPE

NR

CONSTRUCTION MATERIAL SPECIFIC TYPE

NR

** REHEATER

GENERIC TYPE NR
SPECIFIC TYPE NR
TRADE NAME/COMMON TYPE NR
CONSTRUCTION MATERIAL GENERIC TYPE NR
CONSTRUCTION MATERIAL SPECIFIC TYPE NR

** FANS

DESIGN NR
FUNCTION NA
APPLICATION NR
SERVICE NA
CONSTRUCTION MATERIAL GENERIC TYPE NA

** DAMPERS

FUNCTION NR
GENERIC TYPE NR
SPECIFIC TYPE NR
CONSTRUCTION MATERIAL GENERIC TYPE NR
CONSTRUCTION MATERIAL SPECIFIC TYPE NR
LINER GENERIC MATERIAL TYPE NR
LINER SPECIFIC MATERIAL TYPE NR

** DUCTHORK

SHELL GENERIC MATERIAL TYPE NR
SHELL SPECIFIC MATERIAL TYPE NR
LINER GENERIC MATERIAL TYPE NR
LINER SPECIFIC MATERIAL TYPE NR

** REAGENT PREPARATION EQUIPMENT

FUNCTION WET BALL MILL
DEVICE NA
DEVICE TYPE NA

** TANKS

SERVICE NUMBER

BIG RIVERS ELECTRIC: D.B. WILSON 1 (CONT.)

** PUMPS

SERVICE NUMBER

** SOLIDS CONCENTRATING/DEWATERING

DEVICE

*** SLUDGE

** TREATMENT

METHOD FORCED OXIDATION

DEVICE NA
PROPRIETARY PROCESS NA

** DISPOSAL

NATURE NA
TYPE NA
SITE TREATMENT NA

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

9/84 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT INITIAL START-UP OF THE FGD SYSTEM COMMENCED IN SEPTEMBER 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COMPANY NAME PLANT NAME UNIT NUMBER CITY STATE REGULATORY CLASSIFICATION PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW NET UNIT GENERATING CAPACITY W/FGD - MW NET UNIT GENERATING CAPACITY W/FGD - MW EQUIVALENT SCRUBBED CAPACITY - MW	BIG RIVERS ELECTRIC GREEN 1 SEBREE KENTUCKY D 43. (.100 LB/MMBTU) 516. (1.200 LB/MMBTU) 301. (.700 LB/MMBTU) 444 242 222 495 242
** UNIT DATA BOILER AND STACK BOILER SUPPLIER BOILER TYPE BOILER SERVICE LOAD DESIGN BOILER FLUE GAS FLOW - CU.M/S BOILER FLUE GAS TEMPERATURE - C STACK HEIGHT - M STACK TOP DIAMETER - M	BABCOCK & WILCOX PULVERIZED COAL BASE 471.90 (1000000 ACFM) 148.9 (300 F) 107. (350 FT) CONCRETE 4.6 (15.0 FT)
** FUEL DATA FUEL TYPE FUEL GRADE AVERAGE HEAT CONTENT - J/G RANGE HEAT CONTENT BTU/LB AVERAGE ASH CONTENT - % RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - % AVERAGE MOISTURE CONTENT - % AVERAGE SULFUR CONTENT	COAL BITUMINOUS 22795. (9800 BTU/LB) 8200-11800 15.38 9.6-27.5 11.40 5.3-20.1 3.91 2.0-6.0 .05 UNKNOWN
*** PARTICLE CONTROL	
** MECHANICAL COLLECTOR NUMBER TYPE	0 NONE
** ESP NUMBER NUMBER OF SPARES TYPE SUPPLIER INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE - C PRESSURE DROP KPA PARTICLE REMOVAL EFFICENCY - %	2 0 COLD SIDE AMERICAN AIR FILTER 235.9 (500000 ACFM) 148.9 (300 F) .3 (1. IN-H2O) 99.6
** PARTICLE SCRUBBER NUMBER GENERIC TYPE SPECIFIC TYPE TRADE NAME/COMMON NAME SHELL GENERIC MATERIAL SHELL SPECIFIC MATERIAL LINER GENERIC MATERIAL LINER SPECIFIC MATERIAL GAS CONTACTING DEVICE TYPE	0 NONE N/A N/A N/A N/A N/A
*** FGD SYSTEM	

*** FGD SYSTEM

```
** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                            THROWAWAY PRODUCT
   SO2 REMOVAL MODE
                                            WET SCRUBBING
   PROCESS TYPE
                                            LIME
   PROCESS ADDITIVES
                                            MAG
   SYSTEM SUPPLIER
                                            AMERICAN AIR FILTER
   A-E FIRM
                                            BURNS & ROE
                                            FULL SCALE
   DEVELOPMENT LEVEL
   NEW/RETROFIT
                                            NEW
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.00
                                             90.00
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
   CURRENT STATUS
   COMMERCIAL START-UP
                                            12/79
   INITIAL START-UP
                                            12/79
   CONTRACT AWARDED
                                            10/76
** DESIGN AND OPERATING PARAMETERS
                                             4.00
   DESIGN COAL SULFER CONTENT - %
   DESIGN COAL HEAT CONTENT - J/G
                                           23260.0
                                                          ( 10000 BTU/LB)
   DESIGN COAL ASH CONTENT - %
                                             20.00
   DESIGN MOISTURE CONTENT - %
                                              11.25
   DESIGN CHLORIDE CONTENT - %
                                                .05
                                           10869.3
   SPACE REQUIREMENTS - SQ M
                                                         ( 117000 SQ FT)
   OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                             272.0
** QUENCHER/PRESATURATOR
   NUMBER
                                             ດ
   CONSTRUCTION MATERIAL GENERIC TYPE
                                            NR
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                            ND
** ABSORBER
   NUMBER
                                             2
   NUMBER OF SPARES
                                             0
                                            SPRAY TOWER
   GENERIC TYPE
   SPECIFIC TYPE
                                            OPEN COUNTERCURRENT SPRAY
   TRADE NAME/COMMON TYPE
                                            N/A
   SUPPLITER.
                                            AMERICAN AIR FILTER
   DIMENSIONS - FT
                                            34 X 71.5
   SHELL GENERIC MATERIAL
                                            CARBON STEEL
   SHELL SPECIFIC MATERIAL
                                            AISI 1110
   SHELL MATERIAL TRADE NAME/COMMON TYPE
                                            N/A
   LINER GENERIC MATERIAL
                                            ORGANIC
    LINER SPECIFIC MATERIAL
                                           MASTIC
                                          PENNGUARD ADHESIVE
   LINER MATERIAL TRADE NAME/COMMON TYPE
   GAS CONTACTING DEVICE TYPE
                                            NONE
   NUMBER OF CONTACTING ZONES
                                            1
                                           1008.
   LIQUID RECIRCULATION RATE - LITER/S
                                                         (16000 GPM)
                                             4.3
   L/G RATIO - L/CU.M
                                                          ( 32.0 GAL/1000 ACF)
    GAS-SIDE PRESSURE DROP KPA
                                                .4
                                                           ( 1.5 IN-H20)
   SUPERFICAL GAS VELOCITY - M/SEC
                                               2.8
                                                          ( 9.2 FT/S)
    INLET GAS FLOW - CU. M/S
                                             235.95
                                                         ( 500000 ACFM)
                                             148.9
    INLET GAS TEMPERATURE - C
                                                          ( 300 F)
    SO2 REMOVAL EFFICIENCY - %
                                               90.0
** REHEATER
   NUMBER
                                              1
                                              0
   NUMBER OF SPARES
   NUMBER PER MODULE
                                             1
                                            INDIRECT HOT AIR
   GENERIC TYPE
                                            EXTERNAL STEAM HEAT EXCHANGER
   SPECIFIC TYPE
                                            FIN TUBE BUNDLE
   TRADE NAME/COMMON TYPE
                                            HEATED AIR INJECTED INTO BYPASS DUCT
   LOCATION
                                            .0
   PERCENT GAS BYPASSED - AVG
   TEMPERATURE INCREASE - C
                                              13.9
                                                          ( 25 F)
   INLET FLUE GAS FLOW RATE - CU. M/S
                                              75.50 ( 160000 ACFM)
-9.4 ( 15 F)
   INLET FLUE GAS TEMPERATURE - C
   OUTLET FLUE GAS FLOW RATE - CU. M/S
                                             120.81
                                                         ( 256000 ACFM)
   OUTLET FLUE GAS TEMPERATURE C
                                             148.9
                                                          ( 300 F)
   NUMBER OF HEAT EXCHANGER BANKS
                                               3
   NUMBER OF BUNDLES PER BANK
                                               6
```

NUMBER OF TUBES PER BUNDLE 20 NR CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE NR ** FANS 2 NUMBER NUMBER OF SPARES 0 CENTRIFUGAL DESIGN SUPPLIER WESTINGHOUSE FUNCTION UNIT APPLICATION FORCED DRAFT SERVICE DRY FLUE GAS FLOW RATE - CU.M/S 274.80 (582330 ACFM) FLUE GAS TEMPERATURE - C (300 F) 148.9 CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL ** FANS NUMBER 2 NUMBER OF SPARES 0 DESIGN CENTRIFUGAL SUPPLIER WESTINGHOUSE FUNCTION UNIT APPLICATION INDUCED DRAFT SERVICE DRY 274.80 FLUE GAS FLOW RATE CU.M/S (582330 ACFM) FLUE GAS TEMPERATURE - C (300 F) 148.9 CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL ** DAMPERS NUMBER 2 SHUT-OFF FUNCTION GENERIC TYPE GUILLOTINE SPECIFIC TYPE TOP-ENTRY GUILLOTINE/SEAL AIR MANUFACTURER AMERICAN AIR FILTER SERVICE CONDITIONS 350 F/INDEFINITE ** DAMPERS NUMBER 1 FUNCTION SHUT-OFF GENERIC TYPE GUILLOTINE SPECIFIC TYPE TOP-ENTRY GUILLOTINE/SEAL AIR MANUFACTURER AMERICAN AIR FILTER SERVICE CONDITIONS 350 F/INDEFINITE ** DAMPERS NUMBER 1 FUNCTION SHUT-OFF GENERIC TYPE LOUVER SPECIFIC TYPE PARALLEL BLADE MULTILOUVER MANUFACTURER AMERICAN AIR FILTER SERVICE CONDITIONS 350 F/INDEFINITE ** DAMPERS NUMBER 2 SHUT-OFF FUNCTION GENERIC TYPE GUILLOTINE SPECIFIC TYPE BOTTOM ENTRY GUILLOTINE/SEAL AIR MANUFACTURER AMERICAN AIR FILTER MODULATION OPEN SERVICE CONDITIONS 350 F/INDEFINITE CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL CONSTRUCTION MATERIAL SPECIFIC TYPE NR ** DUCTWORK LOCATION ABSORBER INLET CONFIGURATION RECTANGULAR DIMENSIONS 11 X 11 X 43.5 LENGTH SHELL GENERIC MATERIAL TYPE CARBON STEEL SHELL SPECIFIC MATERIAL TYPE AISI 1110 LINER GENERIC MATERIAL TYPE

LINER SPECIFIC MATERIAL TYPE

ORGANIC

MASTIC

```
** DUCTWORK
                                               ABSORBER OUTLET
   LOCATION
   CONFIGURATION
                                               RECTANGULAR
   DIMENSIONS
                                               10 X 10 X 16 LENGTH
    SHELL GENERIC MATERIAL TYPE
                                              CARBON STEEL
    SHELL SPECIFIC MATERIAL TYPE
                                              AISI 1110
    LINER GENERIC MATERIAL TYPE
                                               INORGANIC
    LINER SPECIFIC MATERIAL TYPE
                                               HYDRAULICALLY-BONDED MORTAR
** DUCTWORK
   LOCATION
                                               BYPASS
   CONFIGURATION
                                               RECTANGULAR
   DIMENSIONS
                                               11 X 11 X 64 LENGTH
    SHELL GENERIC MATERIAL TYPE
                                               CARBON STEEL
    SHELL SPECIFIC MATERIAL TYPE
                                              HIGH STRENGTH LOW ALLOY [HSLA]
    LINER GENERIC MATERIAL TYPE
                                               ORGANIC/INORGANIC
    LINER SPECIFIC MATERIAL TYPE
                                               MASTIC/SYNTHETIC BRICK
** REAGENT PREPARATION EQUIPMENT
    FUNCTION
                                               SLAKER
   DEVICE
                                               ND
   DEVICE TYPE
                                               NP
   MANUFACTURER
                                               WALLACE & TIERMAN
    NUMBER
                                                4
    FULL LOAD DRY FEED CAPACITY - M.TONS/HR
                                                   3.6
                                                              ( 4 TPH)
    PRODUCT QUALITY - % SOLIDS
                                                  22.0
** TANKS
                                               NUMBER
    SERVICE
                                                -----
    REACTION
                                                  2
    SCREEN
                                                  2
    THICKENER RETURN WATER
                                                  1
   MIST ELIMINATOR WASH
                                                  1
    ADDITIVE HOLD
                                                  2
    ADDITIVE SURGE
                                                  1
** PUMPS
    SERVICE
                                               NUMBER
    ASSORBER RECIRCULATION
                                                  3
    RECYCLE SLURRY BLEED
    THICKENER UNDERFLOW
                                                  4
    ADDITIVE FEED
                                                  2
    THICKENER RETURN
                                                  2
    SLUDGE FEED
                                                  3
    ADDITIVE SUPPLY
** SOLIDS CONCENTRATING/DEWATERING
                                               VACUUM FILTER
    DEVICE
    NUMBER
                                                3
    NUMBER OF SPARES
                                               1
    DIMENSIONS - FT
                                               12 DIA X 20 LONG
                                               20 TPH [291 GPM AT 25-30% SOLIDS]
    CAPACITY
    SHELL GENERIC MATERIAL TYPE
                                              CARBON STEEL
                                              AISI 1110
    SHELL SPECIFIC MATERIAL TYPE
    LINER SPECIFIC MATERIAL TYPE
                                               NYLON
                                               ORGANIC
    BELT GENERIC MATERIAL TYPE
    BELT SPECIFIC MATERIAL TYPE
                                              POLYPROPYLENE
                                               THICKENER UNDERFLOW
    FEED STREAM SOURCE
                                               25% SOLIDS
    FEED STREAM CHARACTERISTICS
                                               45% SOLIDS
    OUTLET STREAM CHARACTERISTICS
    OVERFLOW STREAM CHARACTERISTICS
                                              1% SOLIDS, 360 GPM
    OUTLET STREAM DISPOSITION
                                               PUG MILL
   OVERFLOW STREAM DISPOSITION
                                               THICKENER
** SOLIDS CONCENTRATING/DEWATERING
   DEVICE
                                               THICKENER
   NUMBER
                                                2
   NUMBER OF SPARES
                                               0
```

CTRCULAR CONFIGURATION 125 DIA X 15.5 DEPTH DIMENSIONS FT 900000 GAL CAPACITY INORGANIC SHELL GENERIC MATERIAL TYPE HYDRAULICALLY-BONDED CONCRETE SHELL SPECIFIC MATERIAL TYPE CARBON STEEL LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE ASTM A-36 [1/4"] BLEED PUMP DISCHARGE 774 GPM, 6% SOLIDS FEED STREAM SOURCE OUTLET STREAM CHARACTERISTICS 774 GPM, 6% SOLIDS
OVERFLOW STREAM CHARACTERISTICS 136 GPM, 25% SOLIDS
OUTLET STREAM CHARACTERISTICS 638 GPM, 1% SOLIDS
OUTLET STREAM DISPOSITION TO VACUUM FILTERS FEED STREAM CHARACTERISTICS 136 GPM, 25% SOLIDS OVERFLOW STREAM DISPOSITION THICKENER RETURN WATER TANK

*** SALEABLE BYPRODUCTS

NATURE NONE
QUALITY - % 25.0

*** SLUDGE

FULL LOAD SLUDGE QUANTITY - M.TONS/HR (DRY) 18.2 (20.0 TPH)
MOISTURE CONTENT - % TOTAL FREE WATER 75.0
% CASO3 - DRY 82.4
% CASO4 - DRY 11.8
% ASH - DRY 5.8

** TREATMENT

METHOD STABILIZATION
DEVICE PUG MILL
PROPRIETARY PROCESS CONVERSION SYSTEMS (POZ-O-TEC)
INLET FLOW RATE - LITER/S 17.1 (272 GPM)
INLET QUALITY - % 25.0

** DISPOSAL

NATURE FINAL
TYPE LANDFILL
LOCATION ON-SITE
SITE TRANSPORTATION METHOD TRUCK
SITE TREATMENT NONE
SITE DIMENSIONS 200 ACRES

** PROCESS CONTROL AND INSTRUMENTATION

PROCESS STREAM ABSORBER RECYCLE CHEMICAL PARAMETERS PH PHYSICAL VARIABLES % SOLIDS CONTROL LEVELS PH 9, 6% SOLIDS MONITOR TYPE LEEDS & NORTHRUP/TEXAS NUCLEAR MONITOR LOCATION SCREEN TANKS PROCESS CONTROL MANNER AUTOMATIC PROCESS CHEMISTRY MODE FEEDBACK

** WATER BALANCE

WATER LOOP TYPE

EVAFORATION WATER LOSS LITER/S

SLUDGE HYDRATICN WATER LOSS - LITER/S

SLUDGE INTERSTITIAL WATER LOSS - LITERS/S

POND SEEPAGE/RUNOFF WATER LOSS - LITERS/S

RECEIVING WATER STREAM

MAKEUP WATER ADDITION - LITERS/S

CLOSED

(12 GPM)

(4 GPM)

N/A

MAKEUP WATER ADDITION - LITERS/S

23.1 (366 GPM)

SOURCE OF MAKEUP WATER COOLING TOWER BLOWDOWN (290 GPM1/RIVER WATER (76

** CHEMICALS AND CONSUMPTION

FUNCTION

ABSORBENT

LIME [THIOSORBIC]

PRINCIPAL CONSTITUENT

SOURCE/SUPPLIER

CONSUMPTION

UTILIZATION - %

ABSORBENT

LIME [THIOSORBIC]

92% CAO, 2-6% INERTS, 2-6% MGO

DRAVO LIME

230 TPD

93.2

POINT OF ADDITION	SLAKER
** FGD SPARE CAPACITY INDICES	
ABSORBER - %	30.0
MIST ELIMINATOR - %	.0
REHEATER - %	.0
FAN - %	.0
THICKENER - %	.0
VACUUM FILTER - %	33.0
** FGD SPARE COMPONENT INDICES	
ABSORBER	.4
MIST ELIMINATOR	.0
REHEATER	.0
FAN	.0
THICKENER	.0
VACUUM FILTER	.1

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

12/79 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD OPERATION COMMENCED IN MID-DECEMBER 1979. THE UNIT OPERATED IN A STARTUP PHASE DURING THIS PERIOD.

1/80 SYSTEM 744 2/80 SYSTEM 696 3/80 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

NO INFORMATION WAS AVAILABLE FOR THE FIRST QUARTER, 1980.

4/80	A	65.0	56.0	78.8	45.0			
	В	65.0	56.0	79.0	45.0			
	SYSTEM	65.0	56.0	79.0	45.0	720	576	324

** PROBLEMS/SOLUTIONS/COMMENTS

THE FOLLOWING FIVE OUTAGES OCCURRED IN APRIL AND ACCOUNTED FOR THE LOW AVAILABILITY OF THE FGD SYSTEM.

- 1. LOW ADDITIVE IN TANK
- 2. INSTRUMENT TROUBLE
- 3. WATER IN THE PANEL
- 4. LOW ON LIME IN THE HOLDING TANKS
- 5. THE ESPS TRIPPED

5/80	A	73.7	76.1	79.0	73.7			
	В	73.7	76. 0	78.9	73.5			
	SYSTEM	73.7	76.1	79.0	73.7	744	72 0	548

** PROBLEMS/SOLUTIONS/COMMENTS

DURING MAY THE FGD SYSTEM WAS OFF LINE FOR APPROXIMATELY 548 HOURS DUE TO THE FOLLOWING PROBLEMS.

- 1. SULFUR OXIDES TOO HIGH
- 2. LOW LEVEL IN ADDITIVE TANK
- 3. INSTRUMENT TROUBLE
- 4. SCHEDULED MAINTENANCE OUTAGE
- 5. SOLIDS ON CARRY OVER
- 6. SOLID WASTE PROBLEM
- 7. UNIT TRIPPED

BIG RIVERS ELECTRIC: GREEN 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

SUZ PART. NOURS NOURS TACTOR

8. CONSTRUCTION WORK

6/80 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS NOT AVAILABLE FOR THE MONTH OF JUNE.

7/80 SYSTEM 744

8/80 SYSTEM 744

9/80 SYSTEM 40.7 720 293

** PROBLEMS/SOLUTIONS/COMMENTS

DURING SEPTEMBER THE VENDOR INSTALLED NEW SWITCHES ON BOTH MODULES'

TRAVELING SCREENS.

10/80 SYSTEM 80.4 40.9 744 304

** PROBLEMS/SOLUTIONS/COMMENTS

ON SEPTEMBER 12 THE FGD SYSTEM WAS TAKEN OFF-LINE FOR A SCHEDULED OUTAGE. THE SYSTEM WAS PLACED BACK IN SERVICE ON OCTOBER 13.

DURING OCTOBER A CONTROL SYSTEM MALFUNCTION CAUSED APPROXIMATELY 2 1/2 DAYS OF OUTAGE TIME.

DUE TO LOST LEVEL IN ADDITIVE HOLD TANK THE SCREW CONVEYOR TRIPPED OUT.

THE THICKENER WAS CLEANED OUT AND THE LEAKS REPAIRED DURING THE MONTH.

LEAKS WERE ENCOUNTERED ON THE EXPANSION JOINTS LOCATED ON THE ABSORBER OUTLET DUCT. THESE EXPANSION JOINTS WERE REPLACED DURING THE MONTH.

11/80 SYSTEM 97.5 96.0 720 691

** PROBLEMS/SOLUTIONS/COMMENTS

A LEAK IN MODULE A BLEED LINE DURING NOVEMBER CAUSED APPROXIMATELY 10 HOURS OF OUTAGE TIME.

12/80 SYSTEM 97.9 93.5 744 695

** PROBLEMS/SOLUTIONS/COMMENTS

DURING DECEMBER SEVEN HOURS OF DOWN TIME WAS DUE TO PROBLEMS AT THE SOLID WASTE FACILITY.

LEAKS WERE ENCOUNTERED WITH THE MIST ELIMINATOR WASH LINES.

PROBLEMS WERE ENCOUNTERED WITH THE CLARIFIERS AT THE COOLING TOWER CAUSING THE FGD SYSTEM TO BE TAKEN OUT OF SERVICE FOR APPROXIMATELY 23 HOURS.

1/81 SYSTEM 88.4 82.9 744 617

** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE FIRST PART OF JANUARY THE UTILITY EXPERIENCED PROBLEMS WITH HAULING THE WASTE PRODUCT. THIS CAUSED THE SYSTEM TO BE TAKEN OFF LINE APPROXIMATELY THREE DAYS.

DURING THE MONTH IT WAS NECESSARY TO WASH THE ID FAN.

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

PROBLEMS WERE ENCOUNTERED WITH THE RECYCLE PUMP PACKING.

2/81 SYSTEM 90.9

84.9

696

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY HAS EXPERIENCED BYPASS DAMPER PROBLEMS AND IN FEBRUARY INSTALLED A SOLENOID ON THE DAMPER TO RESOLVE THE PROBLEM.

REPAIR WORK ON THE MIST ELIMINATOR LEAKS WAS PERFORMED DURING THE MONTH.

THICKENER MAINTENANCE CAUSED AN OUTAGE WHICH LASTED 22 HOURS.

THE ADDITIVE FEED LINE TO MODULE A REACTION TANK PLUGGED.

3/81 SYSTEM 100.0

51.4

744

382

591

** PROBLEMS/SOLUTIONS/COMMENTS

THE SYSTEM WAS SHUT DOWN DURING THE FIRST TWO WEEKS OF MARCH FOR SCHEDULED

MAINTENANCE.

4/81 SYSTEM 100.0

60.7

720

437

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING APRIL.

5/81 SYSTEM 84.7

79.3

744

590

** PROBLEMS/SOLUTIONS/COMMENTS

AT THE FIRST OF MAY GENERAL MAINTENANCE WAS PERFORMED ON THE SYSTEM.

PLUGGING WAS EXPERIENCED IN THE LINES ASSOCIATED WITH THE SLAKER.

THICKENER MAINTENANCE CAUSED THE SYSTEM TO BE OFF-LINE APPROXIMATELY 15 HOURS.

TWO OUTAGES WERE CAUSED BY THE THICKENER RAKE.

A LINE LEAK IN THE MIST ELIMINATOR WASH TANK WAS ENCOUNTERED. FIVE HOURS OF OUTAGE TIME WAS NEEDED TO MAKE THE NECESSARY REPAIRS.

PLUGGED ADDITIVE LINES CAUSED TWO OUTAGES DURING THE MONTH.

6/81 SYSTEM 95.1

95.1

720

684

** PROBLEMS/SOLUTIONS/COMMENTS

DURING JUNE THE ADDITIVE LINES TO BOTH MODULES PLUGGED CAUSING THE SYSTEM TO SHUT DOWN THREE SEPARATE TIMES.

THE BYPASS DAMPER SOLENOID MALFUNCTIONED AND HAD TO BE REPLACED.

PROBLEMS HAVE BEEN ENCOUNTERED WITH THE MODULE B INLET DAMPER.

7/81 A 98.3 96.2 96.2 96.2 96.2 96.2 96.2

SYSTEM 98.3 96.2 96.2 96.2

744 744 716 93.9

BIG RIVERS ELECTRIC: GREEN 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE MAJORITY OF THE OUTAGE TIME DURING THE MONTH RESULTED FROM PLUGGING OF THE ADDITIVE FEED LINES AND CONTROL VALVES, AS WELL AS MECHANICAL PROBLEMS WITH THE LIMIT SWITCHES ON THE DAMPERS.

8/81	A B System	95.2 95.2 95.2	92.6 92.6 92.6	92.6 92.6 92.6	85.3 85.3 85.3	744	686	635	88.9
9/81	A B SYSTEM	84.5 84.5 84.5	96.4 96.4 96.4	96.4 96.4 96.4	79.9 79.9 79.9	720	597	575	71.0

** PROBLEMS/SOLUTIONS/COMMENTS

DURING SEPTEMBER, THE FGD SYSTEM AVAILABILITY WAS SLIGHTLY LIMITED DUE TO THE REPLACEMENT OF THE CHEVRON MIST ELIMINATORS ON BOTH MODULES. THE MIST ELIMINATORS WERE REPLACED DUE TO THEIR NORYL MATERIAL OF CONSTRUCTION WHICH MELTED AT TEMPERATURES GREATER THAN 180 F. THE REPLACEMENT MIST ELIMINATORS ARE CONSTRUCTED OF FIBERGLASS (FIRST STAGE) AND RYTON (SECOND STAGE) RATED FOR TEMPERATURES GREATER THAN 300 F.

10/81	A	75.3	98.3	98.3	74.8				
	В	75.3	98.3	98.3	74.8				
	SYSTEM	75.3	98.3	98.3	74.8	744	566	557	69.7

** PROBLEMS/SOLUTIONS/COMMENTS

DURING OCTOBER A PROBLEM WAS ENCOUNTERED WITH THE BY-PASS SOLENOID CAUSING DOWN TIME.

OUTAGE TIME WAS NECESSARY TO REPAIR LEAKS ON THE INLET DAMPERS AND TO INSPECT THE CHEVRONS.

A LOW PH CAUSED THE ADDITIVE LINE TO MODULE A TO PLUG RESULTING IN AN OUTAGE.

THE BLEED LINE TO MODULE A RUPTURED ACCOUNTING FOR ADDITIONAL DOWN TIME.

11/81	A	96.2	94.9	94.9	94.9				
	В	94.9	94.9	94.9	94.9				
	SYSTEM	95.6	94.9	94.9	94.9	72 0	720	683	97.1

** PROBLEMS/SOLUTIONS/COMMENTS

DURING NOVEMBER THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS OCCURRED.

12/81	A	98.9	97.6	97.6	97.6				
				97.6					
	SYSTEM	98.9	97.6	97.4	97.6	744	744	726	91.2

** PROBLEMS/SOLUTIONS/COMMENTS

DURING DECEMBER NO MAJOR FGD-RELATED PROBLEMS WERE EXPERIENCED.

1/82	A	92.9	90.6	90.6	90.6				
	В	94.8	91.3	91.3	91.3				
	SYSTEM	93.8	91.0	91.0	91.0	744	744	677	88.2

			OPERABILITY	RELIABILITY	UTILIZATI	100	% REI SO2	10VAL PART.	PER HOURS	BOILER HOURS	FGD HOURS	FACTOR
	** PROBLE	MS/SOLUTI	ONS/COMMENTS									
			THE UTILITY RE		NO MAJOR	FGD-	RE LA	TED PR	OBLEMS	WERE E	NCOUNT	ERED
2/82	A	95.4	93.1	93.1	93.1							
	B SYSTEM	97.0 96.2	93.1 93.1	93.1 93.1					672	672	626	87.6
3/82	A	98.4		94.4	93.8							
	B SYSTEM	98.4 98.4	94.4 94.4	94.4 94.4					744	739	698	89.6
			ONS/COMMENTS	, , , , ,	/3.0					,3,	0,0	07.0
	110022	_	DURING FEBRUAR	Y AND MARCH	NO MAJOR	FGD-	RE LA	TED PR	OBLEMS	WERE R	EPORTEI).
/82	A	86.9										
, 02	B	86.9		9 6.4 96.4	58.8							
	SYSTEM	86.9	96.4	96.4	58.8				720	439	423	56.4
/82	A	99.1	98.1	98.1	98.1							
	R	98.1	98.1 98.1	98.1	98.1				7//	744	77.0	
				98.1	98.1				/44	744	730	88.8
	** PROBLE	MS/SOLUTI	ONS/COMMENTS									
			THE UTILITY REDURING APRIL A		NO MAJOR	FGD-	RELA	TED PR	OBLEMS	WERE E	NCOUNT	ERED
/82	G1-A	98.5 98.5	98.5	98.5 98.5	98.5							
	G1-B System		98.5 98.5	98.5 98.5	98.5 98.5				720	720	709	79.8
	** PROBLE	MS/SOLUTI	ONS/COMMENTS									
			THE UTILITY REDURING JUNE.	PORTED THAT	NO MAJOR	FGD-	RELA	TED PR	OBLEMS	WERE E	нсоинті	ERED
7/82	G1-A	98.2		96.2								
	G1-B SYSTEM	98.2 98.2		96.2 96.2	96.2 96.2				744	744	714	93.9
				70.2	70.2				/ 44	/ 77	/10	73.7
	** PRUBLE	MS/SULUII	ONS/COMMENTS									
			PLUGGING OF AD OUTAGE TIME DO		LINES AND	CON	TROL	VALVE	S CONTI	RIBUTED	TO TH	E
			MECHANICAL PRO OUTAGE TIME DO			rches	ON	THE DA	MPERS .	ALSO CO	NTRIBU	TED TO
3/82	G1-A	100.0	99.2	99.2	91.8							
	G1-B SYSTEM	100.0 100.0	99.2 99.2	99.2 99.2	91.8 91.8				744	689	683	70.8
	** PROBLE	MS/SOLUTI	ONS/COMMENTS									
			THE UTILITY REDURING AUGUST.		NO MAJOR	FGD-	RELA	TED PF	OBLEMS	WERE E	NCOUNT	ERED
/82	SYSTEM								720			
/82	SYSTEM								744			

BIG RIVERS ELECTRIC: GREEN 1 (CONT.)

				PERFORMAN	CE DATA						
PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% REN	10VAL	PER	BOILER HOURS	FGD HOURS	CAP. FACTOR

11/82	SYSTEM							720			
12/82	SYSTEM							744			
1/83	SYSTEM							744			
2/83	SYSTEM							672			
3/83	SYSTEM							744			

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE PERIOD OF SEPTEMBER 1982 THROUGH MARCH 1983.

4/83	SYSTEM	720
5/83	SYSTEM	744
6/83	SYSTEM	720

** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE MONTHS OF APRIL AND MAY THE FOLLOWING REPAIRS WERE MADE:

BOTH DOUBLE-LOUVRE SEAL AIR DAMPERS LOCATED AT THE INLET OF THE ABSORBER VESSELS WERE REPLACED WITH BOTTOM-ENTRY GUILLOTINE SEAL AIR DAMPERS. THE DOUBLE-LOUVRE DAMPERS DID NOT PROVIDE ADEQUATE ISOLATION TO ALLOW MAIN-TENANCE DURING BOILER OPERATION. THE UTILITY ALSO REPORTED THAT THE DOUBLE-LOUVRE DAMPERS CLOSED TOO SLOWLY DURING BYPASS (REASON WHY ORIGINAL NORYL MIST ELIMINATORS WERE MELTED). THE FAULTY PRE-KRETE G-8 LINER MATE-RIAL IN THE ABSORBER VESSELS WAS REPLACED WITH PENNGUARD MASTIC. THE PENNGUARD MASTIC WAS APPLIED TO THE ABSORBER AND DUCTWORK FROM THE MIST ELIMINATORS TO THE OUTLET ABSORBER GUILLOTINE DAMPERS. PENNGUARD MASTIC AND PENNGUARD BLOCK WERE BOTH APPLIED TO THE DUCTWORK LOCATED BETWEEN THE OUTLET ABSORBER GUILLOTINE DAMPERS AND THE STACK INLET.

THE UTILITY ALSO REPORTED REDUCING THE L/G RATIO ON BOTH ABSORBER VESSELS (FUMP SPEEDS WERE REDUCED). THE UTILITY REPORTS STILL MEETING COMPLIANCE LIMITS BUT HAVING A 14 PERCENT DECREASE IN LIME USAGE OVER LAST YEAR.

7/83	SYSTEM	744
8/83	SYSTEM	744
9/83	SYSTEM	720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE THIRD QUARTER. THE NEXT SCHEDULED UNIT OUTAGE IS SET TO BEGIN THE FIRST WEEK OF NOVEMBER AND WILL LAST TWO WEEKS.

ABSORBER LIQUID RECIRCULATION WAS DECREASED IN CONJUNCTION WITH CHANGES TO NOZZLE HEADER DESIGN IN ORDER TO SAVE ON LIME CONSUMPTION. THE UTILITY REPORTED THAT THE FGD SYSTEM WAS REMOVING MORE SO2 THAN REQUIRED BY LAW. THE LIQUID RECIRCULATION RATE FOR EACH OF THE TWO ABSORBERS WAS DECREASED FROM A DESIGN FLOW RATE OF 20,280 GPM (L/G OF 40.6) TO 16,000 GPM (L/G OF 32.0). THREE OF THE SIX SPRAY HEADERS ON HALF OF THE PIG TAIL HOZZLES WERE CHANSED TO FULL-FLOW TYPE (BASICALLY A 1-7/8 INCH OPEN HOLE) NOZZLES. DURING NORMAL OPERATIONS 1 PIG TAIL HEADER IS USED IN CONJUNCTION WITH 2 COMBINATION HEADERS. WHEN THESE BECOME PLUGGED, AN ADDITIONAL COMBINATION HEADER IS VALVED IN. WHEN ALL SIX HEADERS ARE USED THE

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

LIQUID RECIRCULATION RATE IS 16,000 GPM. HOWEVER, ONLY THREE OF THE FOUR HEADERS ARE USED FOR NORMAL OPERATING CONDITIONS HAVING A LIQUID RECIRCULATION RATE OF APPROXIMATELY 11,000 TO 13,000 GPM. BECAUSE OF THIS CHANGE THE UTILITY REPORTED SAVING 11,200 TONS OF LIMESTONE AT A SAVINGS OF \$392,000 (COMPARED TO 1982 BASED ON A 9-MONTH PERIOD) WHILE STILL MEETING ITS SOZ LIMITATIONS.

 10/83
 SYSTEM
 744

 11/83
 SYSTEM
 720

 12/83
 SYSTEM
 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURING THE PERIOD. THE UNIT WAS DOWN FOR THE FIRST AND SECOND WEEKS OF NOVEMBER FOR SCHEDULED MAINTENANCE.

DURING 1983, THE UNIT AND FGD SYSTEM OPERATED A TOTAL OF 7854 5 AND 7592.7 HOURS, RESPECTIVELY. TOTAL FGD SYSTEM AVAILABILITY FOR THE YEAR WAS 96.7 PERCENT.

THE AVERAGE COAL SULFUR CONTENT FOR THE YEAR WAS 3.58 PERCENT AND THE LIME TO COAL USAGE RATIO FOR THE YEAR WAS 16:1.

1/84	SYSTEM	744
2/84	SYSTEM	696
3/84	SYSTEM	744
4/84	SYSTEM	720
5/84	SYSTEM	744
6/84	SYSTEM	720
7/84	SYSTEM	744
8/84	SYSTEM	744
9/84	SYSTEM	72 0

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE PENNGUARD BLOCKS INSTALLED IN THE OUTLET DUCT DURING THE SPRING OF 1983 HAVE WORKED FAVORABLY TO DATE.

THE UTILITY REPORTED THAT THE NEW DAMPERS, WHICH HAVE BEEN IN USE 18 MONTHS TO DATE, HAVE OPERATED FAVORABLY.

MIST ELIMINATOR WASH PIPE PLUGGAGE WAS REPORTED. A HIGH PRESSURE WASH (5000 PSI) WAS REQUIRED TO CLEAR THE PLUGGED LINES.

OVERALL FGD SYSTEM AVAILABILITY DURING THE FIRST THREE QUARTERS OF 1984 WAS ESTIMATED AT 90%. NO MAJOR OUTAGES OCCURRED DURING THIS TIME.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

BIG RIVERS ELECTRIC COMPANY NAME GREEN PLANT NAME UNIT NUMBER SEBREE CITY KENTUCKY STATE 43. (.100 LB/MMBTU)
516. (1.200 LB/MMBTU)
301. (.700 LB/MMBTU)
444
242
222 REGULATORY CLASSIFICATION PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NOX EMISSION LITTRICATE
NET PLANT GENERATING CAPACITY - MW
GROSS UNIT GENERATING CAPACITY - MW
NET UNIT GENERATING CAPACITY W/FGD - MW
NET UNIT GENERATING CAPACITY WO/FGD - MW 495 EQUIVALENT SCRUBBED CAPACITY - MW 242 ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER

BOILER TYPE

BOILER SERVICE LOAD

DESIGN BOILER FLUE GAS FLOW - CU.M/S

BOILER FLUE GAS TEMPERATURE - C

STACK HEIGHT - M

CONCRETE

4.6

(1000000 ACFM)

CONCRETE

4.6

(15.0 FT) BOILER SUPPLIER ** FUEL DATA FUEL TYPE COAL FUEL GRADE BITUMINOUS 22795. (9800 BTU/LB) AVERAGE HEAT CONTENT - J/G RANGE HEAT CONTENT - BTU/LB 8200-11800 AVERAGE ASH CONTENT - % 15.38 9.6-27.5 RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - %
RANGE MOISTURE CONTENT - %
AVERAGE SULFUR CONTENT - % 11.40 5.3-20.1 3.91 RANGE SULFUR CONTENT - % 2.0-6.0 AVERAGE CHLORIDE CONTENT - % . 05 RANGE CHLORIDE CONTENT - % UNKNOWN *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER 0 TYPF NONE ** ESP NUMBER 2 NUMBER OF SPARES Ω TYPE COLD SIDE AMERICAN AIR FILTER SUPPLIER INLET FLUE GAS CAPACITY - CU.M/S 235.9 (500000 ACFM)
INLET FLUE GAS TEMPERATURE - C 148.9 (300 F)
PRESSURE DROP - KPA .3 (1. IN-H20)
PARTICLE REMOVAL EFFICENCY - % 99.6 ** PARTICLE SCRUBBER NUMBER 0 GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A N/A SHELL SPECIFIC MATERIAL LINER GENERIC MATERIAL N/A LINER SPECIFIC MATERIAL N/A GAS CONTACTING DEVICE TYPE N/A

*** FGD SYSTEM

```
** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                            THROWAWAY PRODUCT
   SO2 REMOVAL MODE
                                            WET SCRUBBING
   PROCESS TYPE
                                            LIME
   PROCESS ADDITIVES
                                            MAG
   SYSTEM SUPPLIER
                                            AMERICAN AIR FILTER
   A-E FIRM
                                             BURNS & ROE
   DEVELOPMENT LEVEL
                                            FULL SCALE
   NEW/RETROFIT
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.00
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - X
   CURRENT STATUS
   COMMERCIAL START-UP
                                             12/80
   INITIAL START-UP
                                            11/80
   CONTRACT AWARDED
                                             5/77
** DESIGN AND OPERATING PARAMETERS
   DESIGN COAL SULFER CONTENT - %
                                              4.00
   DESIGN COAL HEAT CONTENT - J/G
                                            23260.0
                                                           ( 10000 BTU/LB)
   DESIGN COAL ASH CONTENT - %
                                               20.00
   DESIGN MOISTURE CONTENT - %
                                               11.25
   DESIGN CHLORIDE CONTENT - %
                                                 . 05
   SPACE REQUIREMENTS - SQ M
                                            10869.3
                                                           ( 117000 SQ FT)
   OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                              272.0
** QUENCHER/PRESATURATOR
   NUMBER
                                             0
   CONSTRUCTION MATERIAL GENERIC TYPE
                                            ND
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                            NR
** ABSORBER
   NUMBER
                                             2
   NUMBER OF SPARES
                                              0
                                            SPRAY TOWER
   GENERIC TYPE
   SPECIFIC TYPE
                                            OPEN COUNTERCURRENT SPRAY
   TRADE NAME/COMMON TYPE
                                            N/A
   SUPPLIER
                                            AMERICAN AIR FILTER
   DIMENSIONS - FT
                                             34 X 71.5
   SHELL GENERIC MATERIAL
                                            CARBON STEEL
   SHELL SPECIFIC MATERIAL
                                            AISI 1110
   SHELL MATERIAL TRADE NAME/COMMON TYPE
                                            N/A
                                            ORGANIC
   LINER GENERIC MATERIAL
   LINER SPECIFIC MATERIAL
                                            MASTIC
                                         PENNGUARD ADHESIVE
   LINER MATERIAL TRADE NAME/COMMON TYPE
   GAS CONTACTING DEVICE TYPE
                                            NONE
   NUMBER OF CONTACTING ZONES
                                            1
                                            1008.
   LIQUID RECIRCULATION RATE - LITER/S
                                                           (16000 GPM)
                                             4.3
                                                           ( 32.0 GAL/1000 ACF)
   L/G RATIO - L/CU.M
   GAS-SIDE PRESSURE DROP - KPA
                                                 . 4
                                                          ( 1.5 IN-H20)
   SUPERFICAL GAS VELOCITY - M/SEC
                                               2.8
                                                          ( 9.2 FT/S)
                                                          ( 500000 ACFM)
   INLET GAS FLOW CU. M/S
                                              235.95
   INLET GAS TEMPERATURE - C
                                              148.9
                                                           ( 300 F)
   SO2 REMOVAL EFFICIENCY - %
                                                90.0
** REHEATER
   NUMBER
                                              1
   NUMBER OF SPARES
                                             0
   NUMBER PER MODULE
                                             1
                                            INDIRECT HOT AIR
   GENERIC TYPE
   SPECIFIC TYPE
                                            EXTERNAL STEAM HEAT EXCHANGER
   TRADE NAME/COMMON TYPE
                                            FIN TUBE BUNDLE
                                            HEATED AIR INJECTED INTO BYPASS DUCT
   LOCATION
   PERCENT GAS BYPASSED - AVG
                                                .0
   TEMPERATURE INCREASE - C
                                               13.9
                                                           (
                                                               25 F)
                                              75.50
-9.4
   INLET FLUE GAS FLOW RATE - CU. M/S
                                                           ( 160000 ACFM)
   INLET FLUE GAS TEMPERATURE C
                                                          ( 15 F)
                                            -9.4
120.81
   OUTLET FLUE GAS FLOW RATE - CU. M/S
                                                          ( 256000 ACFM)
   OUTLET FLUE GAS TEMPERATURE - C
                                             148.9
                                                           ( 300 F)
   NUMBER OF HEAT EXCHANGER BANKS
                                                3
   NUMBER OF BUNDLES PER BANK
                                                6
```

LINER SPECIFIC MATERIAL TYPE

20 NUMBER OF TUBES PER BUNDLE CONSTRUCTION MATERIAL GENERIC TYPE ΝR CONSTRUCTION MATERIAL SPECIFIC TYPE NΒ ** FANS 2 NUMBER NUMBER OF SPARES O CENTRIFUGAL DESIGN WESTINGHOUSE SUPPLIER UNIT FUNCTION FORCED DRAFT APPLICATION DRY SERVICE FLUE GAS FLOW RATE - CU.M/S 274.80 (582330 ACFM) FLUE GAS TEMPERATURE - C 148.9 (300 F) CARBON STEEL CONSTRUCTION MATERIAL GENERIC TYPE ** FANS NUMBER 2 NUMBER OF SPARES Λ DESIGN CENTRIFUGAL WESTINGHOUSE SUPPLIER FUNCTION UNIT **APPLICATION** INDUCED DRAFT SERVICE DRY FLUE GAS FLOW RATE - CU.M/S 274.80 (582330 ACFM) FLUE GAS TEMPERATURE - C 148.9 (300 F) CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL ** DAMPERS NUMBER 2 FUNCTION SHUT-OFF GENERIC TYPE GUILLOTINE SPECIFIC TYPE TOP-ENTRY GUILLOTINE/SEAL AIR MANUFACTURER AMERICAN AIR FILTER SERVICE CONDITIONS 350 F/INDEFINITE ** DAMPERS NUMBER 1 FUNCTION SHUT-OFF GENERIC TYPE GUILLOTINE SPECIFIC TYPE TOP-ENTRY GUILLOTINE/SEAL AIR MANUFACTURER AMERICAN AIR FILTER SERVICE CONDITIONS 350 F/INDEFINITE ** DAMPERS NUMBER ì FUNCTION SHUT-OFF GENERIC TYPE LOUVER SPECIFIC TYPE PARALLEL BLADE MULTILOUVER MANUFACTURER AMERICAN AIR FILTER SERVICE CONDITIONS 350 F/INDEFINITE ** DAMPERS NUMBER 2 FUNCTION SHUT-OFF GENERIC TYPE GUILLOTINE SPECIFIC TYPE BOTTOM ENTRY GUILLOTINE/SEAL AIR MANUFACTURER AMERICAN AIR FILTER MODULATION OPEN SERVICE CONDITIONS 350 F/INDEFINITE CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL CONSTRUCTION MATERIAL SPECIFIC TYPE ** DUCTWORK LOCATION ABSORBER INLET CONFIGURATION RECTANGULAR DIMENSIONS 11 X 11 X 43.5 LENGTH SHELL GENERIC MATERIAL TYPE CARBON STEEL SHELL SPECIFIC MATERIAL TYPE AISI 1110 LINER GENERIC MATERIAL TYPE ORGANIC

MASTIC

```
** DUCTWORK
   LOCATION
                                                ABSORBER OUTLET
   CONFIGURATION
                                                RECTANGULAR
   DIMENSIONS
                                                10 X 10 X 16 LENGTH
    SHELL GENERIC MATERIAL TYPE
                                                CARBON STEEL
    SHELL SPECIFIC MATERIAL TYPE
                                                AIST 1110
     LINER GENERIC MATERIAL TYPE
                                                INORGANIC
    LINER SPECIFIC MATERIAL TYPE
                                                HYDRAULICALLY-BONDED MORTAR
** DUCTWORK
    LOCATION
                                                BYPASS
    CONFIGURATION
                                                RECTANGULAR
    DIMENSIONS
                                                11 X 11 X 64 LENGTH
     SHELL GENERIC MATERIAL TYPE
                                                CARBON STEEL
     SHELL SPECIFIC MATERIAL TYPE
                                                HIGH STRENGTH LOW ALLOY [HSLA]
     LINER GENERIC MATERIAL TYPE
                                                ORGANIC
     LINER SPECIFIC MATERIAL TYPE
                                                MASTIC
** REAGENT PREPARATION EQUIPMENT
    FUNCTION
                                                SLAKER
    DEVICE
                                                NR
    DEVICE TYPE
                                                NR
                                                WALLACE & TIERMAN
    MANUFACTURER
    NUMBER
    FULL LOAD DRY FEED CAPACITY - M.TONS/HR
                                                                    4 TPH)
                                                    3.6
                                                                (
    PRODUCT QUALITY - % SOLIDS
                                                   22.0
** TANKS
    SERVICE
                                                NUMBER
    REACTION
                                                   2
    SCREEN
                                                   2
    THICKENER RETURN WATER
                                                   1
    MIST ELIMINATOR WASH
                                                   1
    ADDITIVE HOLD
                                                   2
    ADDITIVE SURGE
** PUMPS
                                                NUMBER
    SERVICE
                                                 ____
    ABSORBER RECIRCULATION
                                                   3
    RECYCLE SLURRY BLEED
                                                   4
    THICKENER UNDERFLOW
                                                   4
    ADDITIVE FEED
                                                   2
    THICKENER RETURN
    SLUDGE FEED
                                                   3
    ADDITIVE SUPPLY
** SOLIDS CONCENTRATING/DEWATERING
    DEVICE
                                                VACUUM FILTER
    NUMBER
                                                 3
    NUMBER OF SPARES
    DIMENSIONS - FT
                                                12 DIA X 20 LONG
                                                20 TPH [291 GPM AT 25-30% SOLIDS]
    CAPACITY
    SHELL GENERIC MATERIAL TYPE
                                                CARBON STEEL
    SHELL SPECIFIC MATERIAL TYPE
                                                AISI 1110
    LINER SPECIFIC MATERIAL TYPE
                                                NYLON
    BELT GENERIC MATERIAL TYPE
                                                ORGANIC
                                                POLYPROPYLENE
    BELT SPECIFIC MATERIAL TYPE
    FEED STREAM SOURCE
                                                THICKENER UNDERFLOW
    FEED STREAM CHARACTERISTICS
                                                25% SOLIDS
    OUTLET STREAM CHARACTERISTICS
                                                45% SOLIDS
    OVERFLOH STREAM CHARACTERISTICS
                                                1% SOLIDS, 360 GPM
    OUTLET STREAM DISPOSITION
                                                PUG MTII
    OVERFLOW STREAM DISPOSITION
                                                THICKENER
** SOLIDS CONCENTRATING/DEWATERING
    DEVICE
                                                THICKENER
    NUMBER
                                                 2
    CONFIGURATION
                                                CIRCULAR
```

POINT OF ADDITION

```
125 DIA X 15.5 DEPTH
    DIMENSIONS - FT
    CAPACTTY
                                                900000 GAL
                                                INORGANIC
     SHELL GENERIC MATERIAL TYPE
                                                HYDRAULICALLY-BONDED CONCRETE
    SHELL SPECIFIC MATERIAL TYPE
                                              CARBON STEEL
ASTM A-36 [1/4"]
BLEED PUMP DISCHARGE
    LINER GENERIC MATERIAL TYPE
    LINER SPECIFIC MATERIAL TYPE
    FEED STREAM SOURCE
    OUTLET STREAM CHARACTERISTICS 136 GPM, 6% SOLIDS
OVERFLOW STREAM CHARACTERISTICS 638 GPM, 1% SOLIDS
OUTLET STREAM DISPOSITION
    OVERFLOW STREAM DISPOSITION
                                                THICKENER RETURN WATER TANK
*** SALEABLE BYPRODUCTS
                                               NONE
    NATURE
    QUALITY - %
                                                   25.0
*** SLUDGE
     FULL LOAD SLUDGE QUANTITY - M.TONS/HR (DRY) 18.2 ( 20.0 TPH)
     MOISTURE CONTENT - % TOTAL FREE WATER
                                                    75.0
    % CASO3 - DRY
                                                    82.4
    % CASO4 DRY
                                                   11.8
     % ASH - DRY
 ** TREATMENT
    METHOD
                                                STABILIZATION
     DEVICE
                                                 PUG MILL
     PROPRIETARY PROCESS
                                                CONVERSION SYSTEMS [POZ-0-TEC]
     INLET FLOW RATE - LITER/S
                                                 17.1 ( 272 GPM)
     INLET QUALITY - X
                                                   25.0
 ** DISPOSAL
    NATURE
                                                FINAL
     TYPE
                                                LANDFILL
     LOCATION
                                                ON-SITE
     SITE TRANSPORTATION METHOD
                                                TRUCK
    SITE TREATMENT
                                                NONE
     SITE DIMENSIONS
                                                200 ACRES
 ** PROCESS CONTROL AND INSTRUMENTATION
    PROCESS STREAM
                                                ABSORBER RECYCLE
     CHEMICAL PARAMETERS
     PHYSICAL VARIABLES
                                                % SOLIDS
    CONTROL LEVELS
                                                PH 9, 6% SOLIDS
    MONITOR TYPE
                                                LEEDS & NORTHRUP/TEXAS NUCLEAR
    MONITOR LOCATION
                                                SCREEN TANKS
     PROCESS CONTROL MANNER
                                                AUTOMATIC
     PROCESS CHEMISTRY MODE
                                                FEEDBACK
 ** WATER BALANCE
    WATER LOOP TYPE
                                                 CLOSED
     EVAPORATION WATER LOSS - LITER/S
                                                            ( 12 GPM)
( 4 GPM)
( 4 GPM)
                                                   .8
                                                    . 3
     SLUDGE HYDRATION WATER LOSS - LITER/S
     SLUDGE INTERSTITIAL WATER LOSS - LITERS/S
                                                     . 3
     POND SEEPAGE/RUNOFF WATER LOSS - LITERS/S 0
     RECEIVING WATER STREAM
                                                N/A
    MAKEUP WATER ADDITION - LITERS/S
                                                           ( 366 GPM)
                                                   23.1
     SOURCE OF MAKEUP WATER
                                                 COOLING TOWER BLOWDOWN [290 GPM]/RIVER WATER [76
 ** CHEMICALS AND CONSUMPTION
    FUNCTION
                                                ABSORBENT
                                                 LIME [THIOSORBIC]
    PRINCIPAL CONSTITUENT
                                                 92% CAO, 2-6% INERTS, 2-6% MGO
     SOURCE/SUPPLIER
                                                DRAVO LIME
    CONSUMPTION
                                                230 TFD
    UTILIZATION %
                                                   93.2
```

SLAKER

** FGD SPARE CAPACITY INDICES

ABSORBER - % 30.0
MIST ELIMINATOR - % .0
REHEATER - % .0
FAN - % .0
THICKENER - % .0
VACUUM FILTER - % 33.0

** FGD SPARE COMPONENT INDICES

ABSORBER .4
MIST ELIMINATOR .0
REHEATER .0
FAN .0
THICKENER .0
VACUUM FILTER .1

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL SO2 PART. HOURS HOURS FACTOR HOURS FACTOR 11/80 SYSTEM 94.2 91.8 720 661

** PROBLEMS/SOLUTIONS/COMMENTS

ON NOVEMBER 14, 1980 OPERATION OF UNIT 2 COMMENCED.

DURING THE MONTH TWO OUTAGES WERE CAUSED BY THICKENER RAKE PROBLEMS.

THE ADDITIVE FEED LINE PLUGGED CAUSING ABOUT EIGHT HOURS OF DOWN TIME.

DURING OPERATION ON LOW RECYCLE FLOW, A WELD ON THE BYPASS DAMPER ADJUSTMENT ARM ROD FAILED.

12/80 SYSTEM 96.2

26.1

744

194

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER WAS DOWN FOR 18 DAYS AT THE BEGINNING OF DECEMBER.

PROBLEMS WITH THE BYPASS DAMPER WAS ENCOUNTERED DURING THE MONTH.

1/81 SYSTEM 94.3

68.1

744

506

** PROBLEMS/SOLUTIONS/COMMENTS

THE DAMPERS MALFUNCTIONED ON MODULE B, WHEN THE RECYCLE PUMP TRIPPED, CAUSING ABOUT SEVEN HOURS OF OUTAGE TIME.

THE UTILITY IS EXPERIENCING PROBLEMS WITH HAULING THE WASTE PRODUCT.

THE MODULE B REACTION TANK HAS EXPERIENCED PLUGGING DUE TO THE INABILITY TO MAINTAIN THE PH.

2/81 SYSTEM 94.5

94.0

696

654

** PROBLEMS/SOLUTIONS/COMMENTS

DURING FEBRUARY THICKENER MAINTENANCE WAS PERFORMED.

3/81 SYSTEM 97.9 97.9 744 728 4/81 SYSTEM 99.9 99.5 720 716

BIG RIVERS ELECTRIC: GREEN 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING MARCH AND APRIL.

5/81 SYSTEM 92.7

92.0

744

684

** PROBLEMS/SOLUTIONS/COMMENTS

THE ADDITIVE LINE TO THE REACTION TANK PLUGGED CAUSING OUTAGE TIME DURING MAY.

6/81 SYSTEM 96.2

95.6

720

688

** PROBLEMS/SOLUTIONS/COMMENTS

THE MODULE A DISCHARGE LINE SEPARATED DURING THE MONTH CAUSING A 10 HOUR OUTAGE.

PROBLEMS WERE ENCOUNTERED WITH THE INLET PRESSURE SWITCH ON BOTH MODULES. THE SWITCHES FOULED APPROXIMATELY SIX TIMES DURING JUNE CAUSING A TOTAL OF 14 HOURS OF OUTAGE TIME.

7/81 A 94.0 89.1 89.1 77.2 B 94.0 89.1 89.1 77.2 SYSTEM 94.0 89.1 89.1 77.2

744 645 574 77.5

** PROBLEMS/SOLUTIONS/COMMENTS

DURING JULY, PLUGGING OF THE ADDITIVE FEED LINES AND CONTROL VALVES, AS WELL AS MECHANICAL PROBLEMS WITH THE LIMIT SWITCHES ON THE DAMPERS CONTRIBUTED TO THE MAJORITY OF THE OUTAGE TIME.

8/81 96.4 94.0 94.0 86.0 97.8 94.0 94.0 86.0 97.1 SYSTEM 94.0 94.0 86.0 640 744 681 85.1 9/81 99.7 98.5 Δ 98.5 98 4 R 99.7 98.5 98.5 98.4 SYSTEM 99.7 98.5 98.5 98.4 720 719 708 84.7

** PROBLEMS/SOLUTIONS/COMMENTS

NO FGD-RELATED PROBLEMS WERE REPORTED FOR THE MONTHS OF AUGUST AND SEPT-EMBER.

10/81 A 76.3 96.2 96.2 72.9 B 76.1 96.2 96.2 72.9 SYSTEM 76.2 96.2 96.2 72.9

744 564 542 66.4

367

320 45.5

** PROBLEMS/SOLUTIONS/COMMENTS

DUPING OCTOBER THE UTILITY REPORTED THAT PROBLEMS WERE ENCOUNTERED WITH A RECYCLE PUMP VALVE.

THE BELT ON THE C MODULE RECYCLE PUMP WAS ADJUSTED ACCOUNTING FOR SOME DOWN TIME.

DURING THE MONTH THE FALL SCHEDULED MAINTENANCE OUTAGE COMMENCED.

11/81 A 62.6 87.4 87.4 44.5 B 62.6 87.4 87.4 44.5 SYSTEM 62.6 87.4 87.4 44.5 720

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE FALL SCHEDULED MAINTENANCE OUTAGE CONTINUED THROUGH THE BEGINNING OF NOVEMBER.

THE ADDITIVE MASS VALVE ON THE A MODULE REACTION TANK WAS REPAIRED.

ADDITIONAL OUTAGE TIME WAS CAUSED BY A BROKEN REHEAT ISOLATION DAMPER DRIVE AND A LEAK IN THE MIST ELIMINATOR MAKE UP.

THE B MODULE ADDITIVE MASS LINE PLUGGED CAUSING A PH DROP.

THE MIST ELIMINATORS WERE REPLACED DUE TO THEIR NORYL MATERIAL OF CONSTRUCTION WHICH MELTED AT TEMPERATURES GREATER THAN 180 F. THE REPLACEMENT MIST ELIMINATORS ARE CONSTRUCTED OF FIBERGLASS (FIRST STAGE) AND RYTON (SECOND STAGE) RATED FOR TEMPERATURES GREATER THAN 300 F.

12/81	A	99.9	98.1	98.1	87. 0				
	В	99.9	98.1	98.1	87.0				
	SYSTEM	99.9	98.1	98.1	87 .0	744	660	647	78.5

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE INCOUNTERED DURING DECEMBER.

		96.5							
•	В	96.8	94.4	94.4	94.4				
		96.6				744	744	705	86.9

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING JANUARY.

2/82	A	99.7	97.8	97.8	97.8			
	В	99.7	97.8	97.8	97.8			
	SYSTEM	99.7	97.8	97.8	97.8	672	672	6 5 7 88.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED EXPERIENCING NO MAJOR FGD-RELATED PROBLEMS DURING FEBRUARY.

3/82	A	39.9	91.9	91.9	39.9			
	В	39.9	91.9	91.9	39.9			
	SYSTEM	39.9	91.9	91.9	39.9	744	323	297 40.5

** PROBLEMS/SOLUTIONS/COMMENTS

DURING MARCH THE SYSTEM WAS TAKEN OFF-LINE PART OF THE TIME FOR A SCHEDULED OUTAGE.

4/82	A	61.8	92.6	92.6	55.6				
	В	61.8	92.6	92.6	55.6				
	SYSTEM	61.8	92.6	92.6	55.6	720	432	401	50.1

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT AND SYSTEM WERE DOWN PART OF APRIL FOR A SPRING OUTAGE.

F /00		00 /	07.0	07.0	00.3
5/82	Α	99.6	97.8	97.8	90.1

	MODULE AV	AILABILITY	OPERABILITY F	RELIABILITY	UTILIZATION	% REI	OVAL PART.	PER HOURS	BOILER HOURS	FGD HOURS	CAP. FACTOR
	В	99.6	97.8 97.8	97.8	90.1						
	SYSTEM	99.6	97.8	97.8	90.1			744	685	671	77.8
	** PROBLE	MS/SOLUTIO	NS/COMMENTS								
		N	O MAJOR FGD-RI	LATED PROBL	EMS WERE REP	PORTED	FOR TI	HE MONT	H OF MA	AY.	
6/82			97.7								
	G2-B System	99.3 99.3	97. 7 97. 7	97.7 97.7	95.9 95.9			720	707	690	80.4
			NS/COMMENTS								
		т	HE UTILITY REI URING JUNE.	PORTED THAT	NO MAJOR FGD	-RELAT	ED PRO	OBLEMS	WERE EN	COUNTE	RED
7/82	G2-A	94.0	89.1	89.1	77.2						
	G2-B SYSTEM	94.0	89.1 89.1	89.1	77.2			766	645	E 7/4	77 E
				07.1	11.2			/44	045	3/4	77.5
	** PRUBLE		NS/COMMENTS								
			LUGGING OF ADI UTAGE TIME DUF		LINES AND CO	INTROL	VALVES	S CONTR	IBUTED	TO THE	
			ECHANICAL PROB UTAGE TIME DUB			S ON T	HE DAI	1PERS A	LSO CON	TRIBUT	ED TO
8/82	G2-A	98.5	98. 5	98.5	98.5						
	G2-B System	98 .5 98 .5	98. 5 98 .5	98.5	98.5 98.5			744	744	733	78.4
	** PROBLE	MS/SOLUTIO	NS/COMMENTS								
			HE UTILITY REI URING AUGUST.	PORTED THAT	NO MAJOR FGD	-RELAT	ED PRO	OBLEMS	WERE EN	COUNTE	RED
9/82	SYSTEM							720			
0/92	SYSTEM										
0/02	3131611							744			
	SYSTEM							744 720			
1/82											
1/82 2/82	SYSTEM							720			
1/82 2/82	SYSTEM SYSTEM							720 744			
1/82 2/82 1/83	SYSTEM SYSTEM SYSTEM							720 744 744			
1/82 2/82 1/83 2/83	SYSTEM SYSTEM SYSTEM SYSTEM SYSTEM	:M S /SOLUTIO	NS/COMMENTS					720 744 744 672			
1/82 2/82 1/83 2/83	SYSTEM SYSTEM SYSTEM SYSTEM SYSTEM	I	NS/COMMENTS NFORMATION WA: 983.	S UNAVAILABL	E FOR THE PE	ERIOD (DF SEP	720 744 744 672 744	1982 TF	HROUGH	MARCH
1/82 2/82 1/83 2/83 3/83	SYSTEM SYSTEM SYSTEM SYSTEM SYSTEM	I	NFORMATION WAS	5 UNAVAILABL	E FOR THE PE	ERIOD (DF SEP	720 744 744 672 744	1982 Tr	HROUGH	MARCH
1/82 2/82 1/83 2/83 3/83	SYSTEM SYSTEM SYSTEM SYSTEM SYSTEM SYSTEM ** PROBLE	I	NFORMATION WAS	5 UNAVAILABL	E FOR THE PE	ERIOD (DF SEP	720 744 744 672 744 TEMBER	1982 Tr	HROUGH	MARCH

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE MONTHS OF APRIL AND MAY THE FOLLOWING REPAIRS WERE MADE:

BOTH DOUBLE-LOUVRE SEAL AIR DAMPERS LOCATED AT THE INLET OF THE ABSORBER VESSELS WERE REPLACED WITH BOTTOM-ENTRY GUILLOTINE SEAL AIR DAMPERS. THE DOUBLE-LOUVRE DAMPERS DID NOT PROVIDE ADEQUATE ISOLATION TO ALLOW MAIN-TENANCE DURING BOILER OPERATION. THE UTILITY ALSO REPORTED THAT THE DOUBLE-LOUVRE DAMPERS CLOSED TOO SLOWLY DURING BYPASS (REASON WHY ORIGINAL NORYL MIST ELIMINATORS WERE MELTED). THE FAULTY PRE-KRETE G-8 LINER MATERIAL IN THE ABSORBER VESSELS WAS REPLACED WITH PENNGUARD MASTIC. THE PENNGUARD MASTIC WAS APPLIED TO THE ABSORBER AND DUCTWORK FROM THE MIST ELIMINATORS TO THE ABSORBER OUTLET GUILLOTINE DAMPERS. PENNGUARD MASTIC AND PENNSUARD BLOCK WILL BE APPLIED DURING THE NEXT MAJOR OUTAGE PERIOD TO THE DUCTWORK LOCATED BETWEEN THE ABSORBER OUTLET GUILLOTINE DAMPERS AND THE STACK INLET.

THE UTILITY ALSO REPORTED REDUCING THE L/G RATIO ON BOTH ABSORBER VESSELS (PUMP SPEEDS WERE REDUCED). THE UTILITY REPORTS STILL MEETING COMPLIANCE LIMITS BUT HAVING A 14 PERCENT DECREASE IN LIME USAGE OVER LAST YEAR.

7/83 SYSTEM 744 8/83 SYSTEM 744 9/83 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

ABSORBER LIQUID RECIRCULATION WAS DECREASED IN CONJUNCTION WITH CHANGES TO NOZZLE HEADER DESIGN IN ORDER TO SAVE ON LIME CONSUMPTION. THE UTILITY REPORTED THAT THE FGD SYSTEM WAS REMOVING MORE SO2 THAN REQUIRED BY LAW. THE LIQUID RECIRCULATION RATE FOR EACH OF THE TWO ABSORBERS WAS DECREASED FROM A DESIGN FLOW RATE OF 20,280 GPM (L/G OF 40.6) TO 16,000 GPM (L/G OF 32.0). THREE OF THE SIX SPRAY HEADERS ON HALF OF THE PIG TAIL NOZZLES WERE CHANGED TO A FULL-FLOW TYPE (BASICALLY A 1-7/8 INCH OPEN HOLE) NOZZLES. DURING NORMAL OPERATIONS 1 PIG TAIL HEADER IS USED IN CON-JUNCTION WITH 2 COMBINATION HEADERS. WHEN THESE BECOME PLUGGED, AN ADDI-TIONAL COMBINATION HEADER IS VALVED IN. WHEN ALL SIX HEADERS ARE USED THE LIQUID RECIRCULATION RATE IS 16,000 GPM. HOWEVER, ONLY THREE OF THE FOUR HEADERS ARE USED FOR NORMAL OPERATING CONDITIONS HAVING A LIQUID RECIRCU-LATION RATE OF APPROXIMATELY 11,000 TO 13,000 GPM. BECAUSE OF THIS CHANGE THE UTILITY REPORTED SAVING 11,200 TONS OF LIMESTONE AT A SAVINGS OF \$392,000 (COMPARED TO 1982 BASED ON A 9-MONTH PERIOD) WHILE STILL MEETING ITS SO2 LIMITATIONS.

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE THIRD QUARTER. THE NEXT SCHEDULED UNIT OUTAGE IS SET TO BEGIN THE FIRST WEEK OF NOVEMBER AND WILL LAST TWO WEEKS.

 10/83
 SYSTEM
 744

 11/83
 SYSTEM
 720

 12/83
 SYSTEM
 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURING THE PERIOD. THE UNIT WAS DOWN FORTHE THIRD AND FOURTH WEEKS OF NOVEMBER FOR SCHEDULED MAINTENANCE.

DURING 1983, THE UNIT AND FGD SYSTEM OPERATED A TOTAL OF 7966.7

BIG RIVERS ELECTRIC: GREEN 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

AND 7742.7 HOURS, RESPECTIVELY. TOTAL FGD SYSTEM AVAILABILITY FOR THE YEAR WAS 97.2 PERCENT.

THE AVERAGE COAL SULFUR CONTENT FOR THE YEAR WAS 3.58 PERCENT AND THE LIME TO COAL RATIO FOR THE YEAR WAS 16:1.

1/84	SYSTEM	744
2/84	SYSTEM	696
3/84	SYSTEM	744
4/84	SYSTEM	720
5/84	SYSTEM	744
6/84	SYSTEM	720
7/84	SYSTEM	744
8/84	SYSTEM	744
9/84	SYSTEM	720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT A NEW OUTLET DUCT LINING (STEBBINS TILE) WAS INSTALLED AT THE OUTLET DUCT MIXING ZONE DURING THE FIRST THREE QUARTERS OF 1984.

THE UTILITY REPORTED THAT THE NEW DAMPERS, WHICH HAVE BEEN IN USE 18 MONTHS TO DATE, HAVE OPERATED FAVORABLY.

MIST ELIMINATOR WASH PIPE PLUGGAGE WAS REPORTED. A HIGH PRESSURE WASH (5000 PSI) WAS REQUIRED TO CLEAR THE PLUGGED LINES.

OVERALL FGD SYSTEM AVAILABILITY DURING THE FIRST THREE QUARTERS OF 1984 WAS ESTIMATED AT 90%. NO MAJOR OUTAGES OCCORRED DURING THIS TIME.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COMPANY NAME PLANT NAME UNIT NUMBER CITY STATE REGULATORY CLASSIFICATION PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW NET UNIT GENERATING CAPACITY W/FGD - MW NET UNIT GENERATING CAPACITY WO/FGD - MW EQUIVALENT SCRUBBED CAPACITY - MW	516. (1.200	LB/MMBTU) LB/MMBTU) LB/MMBTU)
** UNIT DATA - BOILER AND STACK BOILER SUPPLIER BOILER TYPE BOILER SERVICE LOAD DESIGN BOILER FLUE GAS FLOW - CU.M/S BOILER FLUE GAS TEMPERATURE - C STACK HEIGHT - M STACK TOP DIAMETER - M	RILEY STOKER PULVERIZED COAL BASE 717.29 (1520000 135.0 (275 F) 152. (500 F) CONCRETE 5.8 (19.0 F))
** FUEL DATA FUEL TYPE FUEL GRADE AVERAGE HEAT CONTENT - J/G RANGE HEAT CONTENT - BTU/LB AVERAGE ASH CONTENT - % RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - % RANGE MOISTURE CONTENT - % AVERAGE SULFUR CONTENT - % RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - %	COAL BITUMINOUS 24181. (10396 9800-11 9.12 6-18 15.43 13-23 3.40 2.4-4.0 .06 *******	BTU/LB) L000
*** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER TYPE	0 0	
** ESP NUMBER NUMBER OF SPARES TYPE SUPPLIER INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE C PRESSURE DROP - KPA PARTICLE REMOVAL EFFICENCY - % ** PARTICLE SCRUBBER NUMBER GENERIC TYPE SPECIFIC TYPE TRADE NAME/COMMON NAME SHELL GENERIC MATERIAL SHELL SPECIFIC MATERIAL LINER GENERIC MATERIAL LINER SPECIFIC MATERIAL GAS CONTACTING DEVICE TYPE	2 0 COLD SIDE POLLUTION CONTROL-WALTI 358.6 (760001 135.0 (275 1 97.8 0 NONE N/A N/A N/A N/A N/A N/A N/A N/A	D ACFM) F)
WWW ====		

*** FGD SYSTEM

```
** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                               THROWAWAY PRODUCT
                                               WET SCRUBBING
    SO2 REMOVAL MODE
                                               LIMESTONE
   PROCESS TYPE
   PROCESS ADDITIVES
                                               NONE
                                               ENVIRONEERING, RILEY STOKER
   SYSTEM SUPPLIER
                                               GILBERT/COMMONWEALTH ASSOCIATES
    A-E FIRM
   DEVELOPMENT LEVEL
                                               FULL SCALE
    NEW/RETROFIT
                                               NEW
    UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                  85.30
    ENERGY CONSUMPTION - X
                                                   2.9
    CURRENT STATUS
    COMMERCIAL START-UP
                                                8/78
    INITIAL START-UP
                                               7/76
    CONTRACT AWARDED
                                                8/73
** DESIGN AND OPERATING PARAMETERS
    DESIGN COAL SULFER CONTENT - %
                                                  4.00
    DESIGN COAL HEAT CONTENT - J/G
                                               22794.8
                                                             ( 9800 BTU/LB)
    DESIGN COAL ASH CONTENT - %
                                                 18.00
    DESIGN MOISTURE CONTENT - X
                                                  23.00
    DESIGN CHLORIDE CONTENT - X
                                                    .05
    OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                144.0
** QUENCHER/PRESATURATOR
    NUMBER
                                                0
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               ΝR
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               NR
** ABSORBER
   NUMBER
                                               4
    NUMBER OF SPARES
                                               0
    GENERIC TYPE
                                               PACKED TOWER
    SPECIFIC TYPE
                                               ROD DECK
    TRADE NAME/COMMON TYPE
                                               VENTRI-SORBER
    SUPPLIER
                                               ENVIRONEERING, RILEY STOKER
    DIMENSIONS - FT
                                               40.0 X 5.0 X 40.0
    SHELL GENERIC MATERIAL
                                               STAINLESS STEEL; HIGH ALLOY [ATOP ABSORBER]
    SHELL SPECIFIC MATERIAL
                                               AUSTENITIC; NICKEL BASE/CHROMIUM-IRON-COPPER-MOL
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                               TYPE 316L; HASTELLOY G
    LINER GENERIC MATERIAL
                                               NONE
    LINER SPECIFIC MATERIAL
                                               N/A
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                               N/A
    GAS CONTACTING DEVICE TYPE
                                               ROD DECKS
    NUMBER OF CONTACTING ZONES
                                                A
    LIQUID RECIRCULATION RATE LITER/S
                                                 992.
                                                             (15750 GPM)
    L/G RATIO - L/CU.M
                                                  5.9
                                                              ( 44.5 GAL/1000 ACF)
    GAS-SIDE PRESSURE DROP - KPA
                                                  3.0
                                                             (12.0 IN-H20)
    SUPERFICAL GAS VELOCITY - M/SEC
                                                  3.7
                                                             ( 12.0 FT/S)
    INLET GAS FLOW CU. M/S
                                                 167.05
                                                             ( 354000 ACFM)
    INLET GAS TEMPERATURE C
                                                135.0
                                                             ( 275 F)
    SO2 REMOVAL EFFICIENCY - %
                                                  85.3
** MIST ELIMINATOR
    PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                               PRIMARY COLLECTOR
    NUMBER PER SYSTEM
                                                4
   NUMBER OF SPARES PER SYSTEM
                                                0
   NUMBER PER MODULE
                                               1
    GENERIC TYPE
                                               IMPINGEMENT
    SPECIFIC TYPE
                                               BAFFLE
    TRADE NAME/COMMON TYPE
                                               CLOSED VANE
   CONFIGURATION
                                               VERTICAL
    NUMBER OF STAGES
   NUMBER OF PASSES PER STAGE
                                                   3
    FREEBOARD DISTANCE - M
                                                             (12.0 FT)
                                                   3.66
   DISTANCE BETHEEN STAGES - CM
                                                 121.92
                                                              (48.0 IN)
   DISTANCE BETWEEN VANES - CM
                                                  6.3
                                                              ( 2.50 IN)
   VANE ANGLES - DEGREES
                                                 σn
   PRESSURE DROP - KPA
                                                              ( 1.0 IN-H20)
   SUPERFICAL GAS VELOCITY - M/S
```

4.0

(13.0 FT/S)

SPECIFIC TYPE

CONSTRUCTION MATERIAL GENERIC TYPE HIGH ALLOY CONSTRUCTION MATERIAL SPECIFIC TYPE NICKEL BASE/CHROMIUM-IRON-COPPER-MOLYBDENUM WASH WATER SOURCE SUPERNATANT WASH FREQUENCY **EVERY 20 MINUTES** WASH RATE - L/S 102.8 (1630 GAL/MIN) ** REHEATER NUMBER 0 NONE GENERIC TYPE SPECIFIC TYPE N/A TRADE NAME/COMMON TYPE N/A CONSTRUCTION MATERIAL GENERIC TYPE NONE CONSTRUCTION MATERIAL SPECIFIC TYPE N/A ** FANS NUMBER 4 NUMBER OF SPARES 0 DESIGN CENTRIFUGAL SUPPLIER BUFFALO FORGE **FUNCTION** UNIT **APPLICATION** FORCED DRAFT SERVICE DRY FLUE GAS FLOW RATE - CU.M/S 167.05 (354000 ACFM) FLUE GAS TEMPERATURE - C 135.0 (275 F) PRESSURE DROP - KPA 11.6 (38.0 IN-H20) CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL ** DAMPERS NUMBER FUNCTION SHUT-OFF GENERIC TYPE LOUVER SPECIFIC TYPE PARALLEL BLADE MULTILOUVER MANUFACTURER AMERICAN STANDARD SEAL AIR FLOW - CU. M/S 1.96 4150 ACFM) SERVICE CONDITIONS 450 CARBON STEEL CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE AISI 1110 LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DAMPERS NUMBER 8 SHUT-OFF **FUNCTION** GENERIC TYPE GUILLOTINE SPECIFIC TYPE NR ENVIRONMENTAL ELEMENTS MANUFACTURER SEAL AIR FLOW - CU. M/S (1200 ACFM) .57 SERVICE CONDITIONS 450 HIGH ALLOY CONSTRUCTION MATERIAL GENERIC TYPE NICKEL BASE/CHROMIUM-IRON-COPPER-MOLYBDENUM CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DAMPERS NUMBER 1 SHUT-OFF **FUNCTION** GENERIC TYPE LOUVER SPECIFIC TYPE PARALLEL BLADE MULTILOUVER AMERICAN STANDARD **MANUFACTURER** SEAL AIR FLOW - CU. M/S .00 0 ACFM) 450 SERVICE CONDITIONS CONSTRUCTION MATERIAL GENERIC TYPE HIGH ALLOY NICKEL BASE/CHROMIUM-IRON-COPPER-MOLYBDENUM CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DAMPERS NUMBER 1 CONTROL FUNCTION LOUVER GENERIC TYPE

PARALLEL BLADE MULTILOUVER

AMERICAN STANDARD MANUFACTURER 0 ACFM) .00 SEAL AIR FLOW - CU. M/S SERVICE CONDITIONS HIGH ALLOY CONSTRUCTION MATERIAL GENERIC TYPE NICKEL BASE/CHROMIUM-IRON-COPPER-MOLYBDENUM CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE N/A ** DAMPERS NUMBER А CONTROL FUNCTION NΡ GENERIC TYPE SPECIFIC TYPE NR MANUFACTURER BUFFALO FORGE SERVICE CONDITIONS NR NR CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE NR NONE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE N/A ** DAMPERS 4 NUMBER FUNCTION SHUT-OFF GENERIC TYPE LOUVER PARALLEL BLADE MULTILOUVER SPECIFIC TYPE MANUFACTURER AMERICAN STANDARD 1.96 4350 ACEM) SEAL AIR FLOW - CU. M/S SERVICE CONDITIONS 700 NΦ CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE · NR LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DUCTWORK LOCATION TNIFT CONFIGURATION RECTANGULAR SHELL GENERIC MATERIAL TYPE CARBON STEEL SHELL SPECIFIC MATERIAL TYPE AISI 1110 LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DUCTWORK LOCATION **DUTLET & BYPASS** CONFIGURATION CIRCULAR SHELL GENERIC MATERIAL TYPE HIGH ALLOY SHELL SPECIFIC MATERIAL TYPE NICKEL BASE/CHROMIUM-IRON-COPPER-MOLYBDENUM LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DUCTWORK LOCATION TRANSITION DUCT AT BASE OF STACK CIRCULAR TO SQUARE CONFIGURATION SHELL GENERIC MATERIAL TYPE HIGH ALLOY SHELL SPECIFIC MATERIAL TYPE NICKEL BASE/CHROMIUM-IRON-COPPER-MOLYBDENUM LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** REAGENT PREPARATION EQUIPMENT EUNCTION WET BALL MILL DEVICE COMPARTMENTED DEVICE TYPE NR MANUFACTURER KENNEDY VAN SAUN NUMBER 1 NUMBER OF SPARES U FULL LOAD DRY FEED CAPACITY - M.TONS/HR 36.3 (40 TPH) PRODUCT QUALITY - % SOLIDS 35.0

××	TANKS	
	SERVICE	NUMBER
	ABSORBER RECYCLE	·
	WASTE SLURRY BLEED	4
	REAGENT PREP PRODUCT	ī
	MIST ELIMINATOR WASH	4
	MILL SLURRY	1
**	PUMPS	
	SERVICE	NUMBER
	PAUD DEVIDU	
	POND RETURN MIST ELIMINATOR WASH	2 8
	ABSORBER RECIRCULATION	12
	SLURRY TRANSFER	2
	MILL SLURRY	2
××	SOLIDS CONCENTRATING/DEWATERING	
	DEVICE	NONE
~~~	CLUBOR	
***	SLUDGE	
××	TREATMENT	
	METHOD DEVICE	BLEED
	PROPRIETARY PROCESS	N/A N/A
××	DISPOSAL	
	NATURE TYPE	FINAL POND
	LOCATION	ON-SITE
	SITE TRANSPORTATION METHOD	PIPELINE
	SITE TREATMENT	CLAY LINING
	SITE DIMENSIONS SITE CAPACITY - CU.M	57 ACRES 125969 ( 103.0 ACRE-FT)
	SITE SERVICE LIFE - YRS	5
**	PROCESS CONTROL AND INSTRUMENTATION PROCESS STREAM	ABSORBER RECYCLE
	CHEMICAL PARAMETERS	PH
	PHYSICAL VARIABLES	PERCENT SOLIDS, LIQUID LEVEL
	CONTROL LEYELS	PH 6.0 AT INLET, 5.5 AT OUTLET
	MONITOR LOCATION PROCESS CONTROL MANNER	RECYCLE TANK AUTOMATIC
	PROCESS CHEMISTRY MODE	FEEDBACK
**	WATER BALANCE	CLOSED
	WATER LOOP TYPE RECEIVING WATER STREAM	NONE
	MAKEUP WATER ADDITION - LITERS/S	37.8 ( 600 GPM)
**	CHEMICALS AND CONSUMPTION	
	FUNCTION	ABSORBENT
	NAME	LIMESTONE
	PRINCIPAL CONSTITUENT	95% CACO3
	CONSUMPTION UTILIZATION - %	40 TPH 67.0
	POINT OF ADDITION	RECYCLE TANK
,,,,		
**	FGD SPARE CAPACITY INDICES ABSORBER %	.0
	MIST ELIMINATOR - %	.0
	FAN %	.0
	BALL MILL - %	.0
	EFFLUENT HOLD TANK % RECTROULATION PUMP %	.0 33.0
	RECIRCULATION PUMP %	33.0

CENTRAL ILLINOIS LIGHT: DUCK CREEK 1 (CONT.)

** FGD SPARE COMPONENT INDICES

ABSORBER .0
MIST ELIMINATOR .0
FAN .0
BALL MILL .0
EFFLUENT HOLD TANK .0
RECIRCULATION PUMP 4.0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

7/76 SYSTEM

1.1 91.60 744 8

#### ** PROBLEMS/SOLUTIONS/COMMENTS

CONSTRUCTION OF DUCK CREEK 1 BEGAN IN EARLY 1972 AND WAS VIRTUALLY COMPLETED BY SPRING 1976. COMMERCIAL OPERATION WAS INITIATED IN JUNE 1976 WITH THE ESP MODULES IN THE GAS PATH. THE FIRST MODULE OF THE 4-MODULE SCRUBBING SYSTEM WAS INSTALLED BY JUNE 1976 AND START-UP FOR SHAKEDOWN/DEBUGGING PURPOSES OCCURRED IN JULY 1976. THE REMAINING THREE MODULES WILL BE INSTALLED LATER WITH A 4-MODULE START-UP SCHEDULED FOR THE SUMMER OF 1978.

INITIAL OPERATION OF THE FIRST SCRUBBER MODULE FOR SHAKEDOWN AND DEBUGGING PURPOSES OCCURRED DURING THE MONTH. LIMITED SERVICE TIME RESULTED FROM PROBLEMS WITH BAD WELDS, FAULTY PIPE HANGERS, AND ABSORBER LEAKS.

8/76 SYSTEM 2.4 744 18

#### ** PROBLEMS/SOLUTIONS/COMMENTS

LIMITED OPERATIONS CONTINUED THROUGHOUT AUGUST BECAUSE OF THE START-UP AND CONSTRUCTION PROBLEMS MENTIONED FOR JULY, 1976. THE MODULE WAS TAKEN OUT OF THE GAS PATH AT THIS POINT TO CONCENTRATE ON RESOLVING THESE PROBLEM AREAS.

9/76 SYSTEM 50.0 744 360

## ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE RESTART OCCURRED ON SEPTEMBER 9. OPERATION CONTINUED THROUGHOUT THE REMAINDER OF THE MONTH ON AN INTERMITTANT BASIS. MAJOR PROBLEMS INCLUDED PIPE BREAKING, PUMP LINER FAILURES, PLUGGING AND SCALING OF MIST ELIMINATORS, AND SOME BOILER-RELATED PROBLEMS. THE MODULE REMAINED IN SERVICE FOR APPROXIMATELY 15 DAYS OF NON-CONTINUOUS OPERATION. THE ESP MODULES HAVE REMAINED IN SERVICE WITHOUT THE OCCURRENCE OF ANY MAJOR PROBLEMS.

10/76 SYSTEM 51.8 744 385

## ** PROBLEMS/SOLUTIONS/COMMENTS

TOTAL OPERATION TIME DURING THE MONTH WAS APPROXIMATELY 16 DAYS (NON-CONTINUOUS). THE MAJOR PROBLEM AREA WAS THE CONTINUATION OF MASSIVE SCALE DEVELOPMENT ON THE MIST ELIMINATORS, RESULTING IN PLUGGING OF THE PIPING AND NOZZLES TO THE COMPONENTS SPRAY SYSTEM.

11/76 SYSTEM 3.3 720 24

## ** PROBLEMS/SOLUTIONS/COMMENTS

SPORADIC OPERATION RESULTED FROM CONTINUED SCALING PROBLEMS IN THE MIST ELIMINATOR SECTION. RILEY AND CILCO INITIATED MODIFICATIONS TO THE DESIGN OF THE MODULE. SPECIFICALLY, A ROD DECK WAS CHANGED IN THE ABSORBER, PRESSURE DROP ACROSS THE ABSORBER WAS INCREASED, PIPING AND PUMP LINER MATERIALS WERE MODIFIED/REPLACED, AND A FRESH WATER WASH SYSTEM WAS IN-

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS FACTOR

STALLED FOR THE MIST ELIMINATOR.

12/76 SYSTEM .0 744 ß

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE MODULE REMAINED OUT OF SERVICE THE ENTIRE MONTH. DURING THIS TIME, THE BOILER FIRED LOW SULFUR (0.6%) KENTUCKY COAL.

1/77 SYSTEM 744 . 0 2/77 SYSTEM 672 0 0 . 0 .0

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE NO. 1 UNIT WAS DOWN THROUGHOUT THE ENTIRE JANUARY-FEBRUARY PERIOD FOR TURBINE/BOILER OVERHAUL. DURING THE UNIT OUTAGE, A NUMBER OF MODIFICA-TIONS WERE MADE TO THE SCRUBBER.

3/77 SYSTEM 744 47.0 350

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE NO. 1 UNIT WAS RETURNED TO SERVICE IN MID-MARCH. THE SCRUBBER WAS PLACED IN SERVICE TO TEST THE MODIFICATIONS MADE DURING THE PRECEDING OUT-AGE. THESE MODIFICATIONS INCLUDED:

THE MIST ELIMINATOR SPRAY WASH SYSTEM PIPING WAS CHANGED FROM PVC TO FRP MATERIALS. ALSO, AN ADDITIONAL SPRAY HEADER WAS ADDED. THE SLURRY CIRCULATION SYSTEM WAS REVAMPED.

NEOPRENE PUMP LINERS HAVE REPLACED THE ORIGINAL RUBBER LINERS. FLUSH/DRAIN SYSTEMS HAVE BEEN INCLUDED TO MINIMIZE SOLIDS BUILD UP. PIPING VALVES MOVED CLOSER TO THE RECYCLE TANK.

SLURRY STORAGE TANKS EQUIPPED WITH FLUSH/DRAIN SYSTEMS.

ADDITIONAL MIXERS ADDED FOR GREATER AGITATION TO PROMOTE PROCESS CHEMISTRY.

DURING THE LAST PART OF MARCH THE MODULE REMAINED IN SERVICE ON A CONTINUAL BASIS WITH THE EXCEPTION OF A FEW MINOR BOILER OUTAGES. CILCO INTENDS TO CONTINUE EXPERIMENTAL OPERATIONS THROUGHOUT THE APRIL-MAY PERIOD, TESTING THE MECHANICAL MODIFICATIONS AND THE AUTOMATIC CONTROL LOOPS (SYSTEM CHEMISTRY WILL BE CONTROLLED BY INLET/OUTLET SO2 LOADING, SOLUTION PH, SOLUTION SOLIDS. OPERATION UP TO THIS POINT HAS PROCEEDED IN A MANUAL CONTROL MODE). CONTINUED OPERATION BEYOND THIS TIME FRAME WILL DEPEND UPON THE SUCCESS OF EXPERIMENTAL OPERATIONS. CILCO HAS THE OPTION OF FIRING LOW SULFUR COAL UNTIL THE ENTIRE 4-MODULE SCRUBBER PLANT IS READY FOR SERVICE IN AUGUST 1978.

4/77	SYSTEM	.0	720	0
5/77	SYSTEM	.0	744	0
6/77	SYSTEM	.0	720	0
7/77	SYSTEM	.0	744	0
8/77	SYSTEM	.0	744	0
9/77	SYSTEM	.0	720	0
10/77	SYSTEM	.0	744	0
11/77	SYSTEM	.0	720	0
12/77	SYSTEM	.0	744	0
1/78	SYSTEM	.0	744	0

CENTRAL ILLINOIS LIGHT: DUCK CREEK 1 (CONT.)

			PERFORMAI	NCE DATA		 				
PERIOD	MODULE	AVAILABILITY			% REI		BOILER HOURS	FGD HOURS	CAP. FACTOR	
2/78	SYSTEM			.0		672		0		
3/78	SYSTEM			.0		744		0		
4/78	SYSTEM			.0		720		0		
5/78	SYSTEM			.0		744		0		
6/78	SYSTEM			.0		720	0	0	.0	

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT CONTINUED TO FIRE LOW-SULFUR COLORADO COAL DURING THE REPORT PERIOD. THE RESTART OF SCRUBBER OPERATIONS CONTINUES TO BE SCHEDULED FOR AUGUST 1978.

7/78 SYSTEM

720

## ** PROBLEMS/SOLUTIONS/COMMENTS

ALL FOUR MODULES BECAME OPERATIONAL ON JULY 24.

MODIFICATIONS WERE MADE TO THE UNDER DESIGNED SLURRY TRANSFER TANK.

A PLUGGING PROBLEM CAUSED BY COAL FINES IN THE SLURRY WAS EXPERIENCED. THE FINES RESULTED FROM A COMMON COAL AND LIMESTONE HANDLING SYSTEM.

8/78	SYSTEM	45.0	46.0	46.0	42.0	744	691	315	62.5
9/78	SYSTEM	46.0	46.0	46.0	44.0	720	691	317	62.5

## ** PROBLEMS/SOLUTIONS/COMMENTS

SCREEN BASKETS WERE USED TO KEEP COAL PARTICLES FROM THE LIMESTONE. THE COAL PARTICLES RESULT FROM THE COMMON COAL-LIMESTONE HANDLING SYSTEM.

THE SLURRY TRANSFER SYSTEM PREVENTED PROPER SLURRY FLOW DUE TO UNDER DESIGN. THE OLD SYSTEM WAS REPLACED WITH A NEW PIPING SYSTEM.

PLUGGING OF THE RECYCLE PUMP SHUT-OFF VALVES OCCURED. THE VALVES ARE BEING REPLACED WITH PINCH VALVES.

THE SCRUBBER WASTE WATER SUMP PUMPS HAVE BEEN PLUGGING. NEW PUMPS ARE BEING INVESTIGATED.

10/78	A	19.1	31.6	31.6	19.1				
	В	22.5	37.2	37.2	22.5				
	С	.8	1.3	1.3	.8				
	D	20.5	33.9	33.9	20.5				
	SYSTEM	15.7	26.0	26.0	15.7	744	449	117	32.9

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE MAJOR CAUSES FOR DOWNTIME OCCURRING IN OCTOBER WERE VALVE LEAKS AND SUBSEQUENT RECYCLE GLAND SEAL CONTAMINATION AND THE INSTALLATION OF A LIQUID/SOLID SEPARATOR.

A LEAKING VALVE RESULTED IN CONTAMINATION OF THE RECYCLE PUMP GLAND SEAL_WATER SYSTEM WITH POND RETURN WATER CAUSING SCALING AND PLUGGING FORCING SHUTDOWN OF THE RECYCLE PUMPS. A NEW VALVE SYSTEM WAS INSTALLED AND THE OPERATING PRESSURES WERE CHANGED TO PREVENT RECURRANCE OF THE CONTAMINATION.

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

THE RECYCLE PUMPS WERE SHUT DOWN WHEN CONTAMINATION OF THE GLAND SEAL WATER SYSTEM CAUSED BY A FAULTY VALVE OCCURRED.

A FLOW CONTROL VALVE ON THE D-MODULE WAS REMOVED BECAUSE IT CAUSED ABRASION AND FAILURE OF THE RECYCLE HEADER. NONE OF THE MODULES NOW UTILIZE FLOW CONTROL VALVES.

THE MIST ELIMINATOR SPRAY NOZZLES PLUGGED BY COAL PARTICLES WERE CLEANED THE COAL PARTICLES RESULT FROM A COMMON COAL/LIMESTONE HANDLING SYSTEM. A LIQUID/SOLID SEPARATOR HAS BEEN INSTALLED IN THE SLURRY SYSTEM TO PREVENT RECURRENCE.

EXCESSIVE LIMESTONE CARRYOVER TO THE MIST ELIMINATOR WAS NOTED. THE TOP ROD DECK WAS REMOVED TO IMPROVE GAS FLOW AND ELIMINATE THE CARRYOVER PROBLEM.

BLANK OFF PLATES WERE ADDED TO THE LOWER SEVEN ROD DECKS TO MAINTAIN PRESSURE DROP REQUIREMENTS. THIS HAS BEEN FOUND TO BE AN ACCEPTABLE SOLUTION AT OTHER ENVIRONEERING FGD SYSTEM INSTALLATIONS.

11/78	A	8.1	8.8	8.8	8.1				
	В	8.1	8.8	8.8	8.1				
	С	8.1	8.8	8.8	8.1				
	D	8.1	8.8	8.8	8.1				
	SYSTEM	8.1	8.8	8.8	8.1	720	661	59	63.6

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE 1B SLURRY TANK PUMP LINER EXPERIENCED A FAILURE RESULTING IN SCRUBBING SYSTEM SHUTDOWN FOR 84 HOURS. THE LINER FAILED AFTER ONLY THREE MONTHS. THE SPARE PUMP WAS ALREADY OUT OF SERVICE FOR A MOTOR REPLACEMENT.

A SPARE SLURRY TANK PUMP WAS OUT OF SERVICE TO REPLACE THE ORIGINAL 50-HP MOTOR WITH A 75-HP MOTOR.

THE PINION BEARING ON THE BALL MILL DRIVE FAILED. THE FAILURE IS BEING INVESTIGATED. FGD SYSTEM OPERATION WAS HALTED DUE TO THE FAILURE. THIS ACCOUNTED FOR MOST OF THE NOVEMBER OUTAGE TIME.

THE LEVEL AND DENSITY INSTRUMENTS ON RECYCLE TANKS ARE BEING MODIFIED.

THE LEEDS & NORTHRUP LEVEL AND DENSITY TRANSMITTERS ARE BEING REPLACED WITH ROSEMOUNT TRANSMITTERS.

12/78	A	23.3	24.5	24.5	23.3				
	В	26.2	27.6	27.6	26.2				
	C	21.3	22.5	22.5	21.3				
	D	10.2	10.8	10.8	10.2				
	SYSTEM	20.3	21.4	21.4	20.3	744	706	151	70.3

## ** PROBLEMS/SOLUTIONS/COMMENTS

ISOLATION DAMPER FAILURES AND SLURRY RECYCLE DISCHARGE VALVE FAILURES OCCURRED DURING DECEMBER.

LIMESTONE MILL PROBLEMS AND A PLUGGED LIMESTONE FEEDER HAMPERED SCRUBBER OPERATIONS DURING DECEMBER.

THE SYSTEM EXPERIENCED FROZEN INSTRUMENT CONTROL LINES IN DECEMBER. THIS WAS THE MAJOR CAUSE OF THE DECEMBER SCRUBBER UNAVAILABILITY.

1/79 SYSTEM .0 .0 .0 .0 .744 738 0 77.0

CENTRAL ILLINOIS LIGHT: DUCK CREEK 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

## ** PROBLEMS/SOLUTIONS/COMMENTS

FROZEN INSTRUMENT CONTROL LINES, RECYCLE TANK SUCTION LINES, MAIN MODULE DRAIN LINES AND MIST ELIMINATOR DRAIN LINES WERE MAJOR PROBLEM AREAS DURING JANUARY.

SLURRY RECYCLE VALVE PLUGGING AND SLURRY TRANSFER PUMP FAILURE CONTRIBUTED TO THE SYSTEM OUTAGE TIME.

2/79 SYSTEM .0 .0 .0 .0 672 533 0 63.8

## ** PROBLEMS/SOLUTIONS/COMMENTS

RECYCLE PUMP SUCTION VALVE FAILURES AND A SLURRY TRANSFER PUMP FAILURE CONTRIBUTED TO THE NON-OPERATION OF THE FGD SYSTEM.

FROZEN MIST ELIMINATOR DRAINS, ABSORBER DRAINS AND INSTRUMENT LINES WERE A MAJOR PROBLEM DURING FEBRUARY.

3/79	A	33.7	31.1	31.1	31.1			
	В	6.7	6.7	6.7	6.7			
	С	.0	.0	.0	. 0			
	D	. 0	.0	. 0	.0			
	SYSTEM	10.1	9.5	9.5	9.5	744	744	70

#### ** PROBLEMS/SOLUTIONS/COMMENTS

FREEZING PROBLEMS CONTINUED TO HAMPER FGD OPERATIONS DURING MARCH. THE C AND D MODULE WERE STILL NOT BACK IN SERVICE DUE TO MAJOR CLEAN-UP FROM THE FREEZING PROBLEMS.

BROKEN MIST ELIMINATOR SPRAY LINES AND PLUGGED MIST ELIMINATOR NOZZLES WERE PROBLEM AREAS DURING MARCH.

RECYCLE PUMP FAILURES AND WASTE WATER PUMP FAILURES WERE EXPERIENCED DURING MARCH.

PLUGGED SLURRY NOZZLES AND GENERAL INSTRUMENTATION PROBLEMS WERE REPORTED BY THE UTILITY.

4/79	A	100.0	71.9	100.0	67.3				
	В	84.3	50.5	75.0	47.3				
	С	86.5	81.2	84.9	76.0				
	D	21.3	22.7	21.3	21.3				
	SYSTEM	73.0	56.6	70.3	53.0	720	674	380	55.9

## ** PROBLEMS/SOLUTIONS/COMMENTS

INLET DAMPER MALFUNCTIONS HINDERED FGD OPERATION DURING APRIL.

PLUGGED MIST ELIMINATOR SPRAY NOZZLES DURING APRIL HINDERED FGD OPERATION.

SLURRY CONTROL VALVE MALFUNCTIONS WERE REPORTED BY THE UTILITY.

RECYCLE TANK MIXER FAILURES WERE EXPERIENCED DURING APRIL.

RECYCLE PUMP BELT AND BEARING FAILURES AND SLURRY SUPPLY LINE FAILURES WERE REPORTED BY THE UTILITY.

5/79	A	95.7	37.4	69.7	9.9
	В	95.7	44.2	73.2	11.7
	С	94.7	41.8	71.1	11.1

			PERFORMAL	NCE DATA					
	E AVAILABILITY								CAP.
, chizes were					SO2 PART				FACTOR
ם	1.3	5.0	1.3	1.3					
SYSTE	M 71.9	32.1	53.8	8.5		744	197	63	14.8

## ** PROBLEMS/SOLUTIONS/COMMENTS

MIST ELIMINATOR PUMP MALFUNCTIONS WERE REPORTED DURING MAY. MODULE D WAS UNAVAILABLE DUE TO A MIST ELIMINATOR WASH LINE FAILURE.

MILL SHAKER BASKET DRIVE MOTOR FAILURES WERE ENCOUNTERED.

SLURRY SUPPLY LINE FAILURES OCCURRED DURING THE MONTH.

STACK LINER BLISTERING WAS DISCOVERED DURING A SPRING INSPECTION. REPAIRS WERE MADE. THE STACK WILL BE INSPECTED AGAIN IN MARCH 1980.

6/79	A	81.9	76.9	79.6	70.6				
	В	89.2	86.9	88.1	79.8				
	С	86.6	83.0	85.1	76.2				
	D	92.0	90.0	91.1	82.7				
	SYSTEM	87.4	84.2	86.0	77.3	720	661	557	70.0

## ** PROBLEMS/SOLUTIONS/COMMENTS

DURING JUNE SOME PROBLEMS WITH THE MIST ELIMINATOR WERE ENCOUNTERED. THESE PROBLEMS INCLUDED PLUGGING IN THE MIST ELIMINATOR AND THE MIST ELIMINATOR LINES AND A BROKEN MIST ELIMINATOR RETURN LINE.

THE UTILITY REPORTED STORAGE PUMP LEAKS, RECYCLE PUMP FAILURES, SLURRY SUPPLY LINE PLUGGING AND DAMPER AND MILL SHAKER BASKET FAILURES.

7/79	A	93.1	85.6	89.7	59.9				
	В	94.9	88.3	92.3	61.7				
	С	95.8	87.9	93.6	61.5				
	D	96.1	86.4	93.9	60.4				
	SYSTEM	95.0	87.1	92.4	60.9	744	520	453	48.7

## ** PROBLEMS/SOLUTIONS/COMMENTS

IN JULY THE MIST ELIMINATOR PLUGGED CAUSING OPERATIONAL PROBLEMS.

RECYCLE PUMP FAILURES WERE ENCOUNTERED DURING THE PERIOD.

8/79 A	3.0	4.0	3.0	3.0			
В	26.1	31.4	24.0	23.4			
С	13.6	18.3	13.6	13.6			
ם	9.5	12.7	9.5	9.5			
SYSTEM	13.1	16.6	12.5	12.4	744	555	92 53.8

## ** PROBLEMS/SOLUTIONS/COMMENTS

IN AUGUST THE MIST ELIMINATOR AND THE MIST ELIMINATOR DRAIN LINES PLUGGED CAUSING EXTENSIVE DOWNTIME FOR MODULE CLEANING.

FAILURES WITH THE LIMESTONE SLURRY FORWARDING PUMP AND THE RECYCLE PUMP WERE ENCOUNTERED.

DAMPER MALFUNCTIONS WERE REPORTED BY THE UTILITY.

9/79 A	63.9	53.9	58.0	49.8				
В	61.2	48.4	53.5	44.7				
С	49.0	38.9	41.4	35.9				
D	88.8	86.2	87.6	79.6				
SYSTE	M 65.7	56.9	60.1	52.5	720	665	378	69.1

CENTRAL ILLINOIS LIGHT: DUCK CREEK 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

#### ** PROBLEMS/SOLUTIONS/COMMENTS

PLUGGING IN THE MIST ELIMINATOR, MIST ELIMINATOR HEADER AND NOZZLES WERE ENCOUNTERED IN AUGUST CONTINUED IN SEPTEMBER.

THE DAMPER FAILED CAUSING A PROBLEM DURING SEPTEMBER.

THE UTILITY REPORTED MIST ELIMINATOR PUMP CAVITATION PROBLEMS RELATED TO MIST ELIMINATOR PROBLEMS ENCOUNTERED IN AUGUST.

PLUGGED SLURRY NOZZLES AND LIMESTONE CONVEYOR FAILURES CONTRIBUTED TO THE OUTAGES EXPERIENCED.

SCRUBBER UNAVAILABILITY WAS PRIMARILY A RESULT OF CARRY-OVER PLUGGING PROBLEMS FROM AUGUST AND SUBSEQUENT CLEAN-UP.

10/79	A	84.8	82.3	89.2	82.3
	В	93.7	86.2	92.4	86.2
	С	91.7	75.8	90.5	75.8
	D	93.5	91.9	93.4	91.9
	SYSTEM	90.9	84.1	91.4	84.1

## ** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE MONTH OF OCTOBER PROBLEMS WERE ENCOUNTERED WITH THE MIST ELIMINATOR SECTIONS. THE MIST ELIMINATOR PUMP MALFUNCTIONED, THE LINES PLUGGED AND A HEADER FLANGE GASKET FAILED.

744 744

720 583 221 61.2

625 72.4

OUTAGE TIME RESULTED FROM THE MODULE ISOLATION DAMPER FAILURE INCLUDING DAMPER MOTOR MALFUNCTION.

THE SLURRY SUPPLY LINE NEEDED REPAIRS.

11/79	A	43.1	52.1	52.1	42.2	
	В	12.4	15.3	18.8	12.4	
	С	22.4	22.6	24.9	18.3	
	D	51.0	61.9	62.0	50.1	
	SYSTEM	32.2	38.0	39.5	30.8	

## ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE ISOLATION DAMPER PROBLEMS CONTINUED DURING NOVEMBER.

THE MIST ELIMINATOR AND THE MIST ELIMINATOR DRAIN PLUGGED CAUSING DOWN TIME.

ALL RECYCLE PUMP SUCTION VALVES WERE REPLACED DURING THE MONTH. THIS WAS THE PRIMARY CAUSE FOR THE LOW SYSTEM AVAILABILITY.

SLURRY SUPPLY LINES FAILED AGAIN, DURING NOVEMBER.

12/79	A B C	54.5 35.1 43.0	72.6 47.6 58.4	77.6 51.0 61.9	53.5 35.1 43.0				
	D	25.5	34.6	40.9	25.5				
	SYSTEM	39.5	53.3	57.9	39.3	744	548	292	60.8

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE ISOLATION DAMPER FAILURES CONTINUED.

THE MIST ELIMINATOR PROBLEMS WITH PLUGGING AND HEADER RUPTURES OCCURRED DURING DECEMBER.

# PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS FACTOR

THE MODULE B AND D RECYCLE TANK LINERS WERE REPAIRED AND TANK COVERS WERE INSTALLED.

MIST ELIMINATOR PLUGGING AND RECYCLE TANK REPAIRS ACCOUNTED FOR MOST OF THE DECEMBER SCRUBBER OUTAGE TIME.

1/80	A	24.8	27.0	29.8	24.8
	В	58.5	63.6	65.9	58.5
	С	17.1	18.6	20.3	17.1
	D	29.2	31.8	35.3	29.3
	SYSTEM	32.4	35.3	37.8	32.4

744 684 241 81.6

342 73.5

## ** PROBLEMS/SOLUTIONS/COMMENTS

MOST OF THE JANUARY OUTAGE TIME WAS REQUIRED FOR RECYCLE TANK COVERING WORK.

THE MIST ELIMINATOR SECTION PLUGGED ALONG WITH THE NOZZLES HINDERING SYSTEM OPERATIONS. THE MIST ELIMINATOR DRAIN LINE WAS MODIFIED ALSO CAUSING OUTAGE TIME.

OTHER PROBLEMS ENCOUNTERED DURING THE MONTH INCLUDED A PLUGGED LIMESTONE FEEDER, INLET DAMPER PROBLEMS, SLURRY SUPPLY HEADER LEAKS AND STORAGE PUMP DISCHARGE VALVE REPAIRS.

2/80	A	11.8	11.8	12.5	11.8			
	В	72.7	72.7	73.5	72.7			
	С	70.7	70.7	71.5	70.7			
	D	41.3	41.3	47.9	41.3			
	SYSTEM	49.1	49.1	51.4	49.1	696	696	

## ** PROBLEMS/SOLUTIONS/COMMENTS

DURING FEBRUARY SOME OUTAGE TIME WAS DUE TO MODULE D CLEANING AND THE CLEANING OF THE MODULE D MIST ELIMINATOR SECTION.

THE INLET DAMPER DRIVE WAS REPLACED DURING THE MONTH.

REPAIR OF THE FIBERGLASS ON THE SLURRY RECYCLE LINE HINDERED OPERATIONS DURING THIS MONTH.

THE MODULES A AND D RECYCLE DISCHARGE VALVE WERE REPLACED CAUSING EXTENSIVE DOWN TIME.

3/80	A	52.9	62.5	64.7	52.9				
	В	73.2	86.6	86.9	73.2				
	С	51.0	60.3	60.5	51.0				
	D	34.0	40.2	45.9	34.0				
	SYSTEM	52.8	62.4	65.1	52.8	744	629	393	68.6

## ** PROBLEMS/SOLUTIONS/COMMENTS

DURING MARCH NEW RECYCLE PUMP DISCHARGE VALVES WERE INSTALLED IN ORDER TO ELIMINATE RESTRICTED FLOW OF THE OLD VALVES.

CARRIER BEARINGS ON THE INLET DAMPER WERE REPLACED IN ORDER TO MAINTAIN MODULE ISOLATION CAPABILITY.

THE MIST ELIMINATOR WASH SYSTEM WAS CONVERTED TO RETURN WATER IN ORDER TO ACHIEVE A HIGHER QUALITY ELIMINATION WASH WATER.

FIBERGLASS LINES ON THE RECYCLE PUMP DISCHARGE WERE ALSO REPAIRED DURING EXTENSIVE

CENTRAL ILLINOIS LIGHT: DUCK CREEK 1 (CONT.)

				PERFORMAL	NCE DATA						
		AVAILABILITY				% REN	10 V A L	PER	BOILER	FGD	CAP. FACTOR
4/80	A	53.0	81.7	95.9	52.9						
	В	54.2	83.6	87.5	54.2						
	С	57.2	88.3	95.3	57.2						
	D	26.0	40.1	71.9	26.0						
	SYSTEM	47.6	73.4	89.2	47.6			720	466	342	35.3

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE MAJOR PROBLEM HINDERING SYSTEM OPERATIONS DURING APRIL WAS THE REBUILD OF THE RECYCLE TANK MIXER.

MINOR PROBLEMS DURING THE MONTH WERE CAUSED BY THE INOPERABILITY OF THE LIMESTONE HANDLING SYSTEM.

5/80	A	44.6	68.6	72.0	44.6				
	В	45.7	70.3	73. <b>5</b>	45.7				
	С	34.7	53.3	59.1	34.7				
	D	43.6	67.0	73.9	43.6				
	SYSTEM	42.1	64.8	69.7	42.1	744	484	314	49.4

## ** PROBLEMS/SOLUTIONS/COMMENTS

DURING MAY REPAIRS WERE MADE TO THE RECYCLE TANK RUBBER LINER.

EXPANSION JOINT LEAKS WERE ALSO REPAIRED DURING THE MONTH.

OTHER OPERATIONAL PROBLEMS INCLUDED THE REPLACEMENT OF THE LIMESTONE STORAGE TANK MIXER MOTOR, MODIFICATION OF ROD DECKS TO REDUCE SYSTEM DIFFERENTIAL PRESSURE AND REPAIR OF THE LIMESTONE FEEDER SYSTEM.

6/80	A	87. <b>6</b>	82.3	87.1	82.1				
	В	86.8	82.6	86.0	82.3				
	С	84.5	81.4	84.3	81.1				
	ם	80.0	73.1	75.8	72.9				
	SYSTEM	84.8	79.9	84.3	79.6	720	718	573	78.5

## ** PROBLEMS/SOLUTIONS/COMMENTS

A LEAK WAS REPAIRED IN THE SLURRY SUPPLY HEADER DURING JUNE.

WORK CONTINUED ON THE MODIFICATIONS BEING DONE ON THE ROD DECKS IN THE ABSORBER MODULES.

7/80	A	91.2	81.0	87.6	70.1				
	В	83.5	70.0	80.0	60.6				
	С	90.5	78.8	86.4	68.2				
	D	87.5	74.9	85.4	64.8				
	SYSTEM	88.2	76.2	84.9	65.9	744	644	490	67.4

## ** PROBLEMS/SOLUTIONS/COMMENTS

DURING JULY FGD SYSTEM OUTAGE TIME RESULTED FROM THE NECESSARY REPAIR OF THE SLURRY SUPPLY LINE AND REPAIR OF THE MALFUNCTIONING CLUTCH IN THE MILL SYSTEM.

ADDITIONAL OUTAGE TIME OCCURRED SO REPAIRS TO THE 1B STORAGE TANK PUMP DISCHARGE VALVES AND THE STORAGE TANK MIXER MOTOR COULD BE COMPLETED.

8/80	A	88.6	85.4	92.7	81.9				
	В	91.4	86.3	90.8	82.7				
	С	91.3	84.6	88.9	81.0				
	D	90.6	85.1	90.1	81.6				
	SYSTEM	90.5	85.4	90.7	81.9	744	713	609 76.5	

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE SLURRY SUPPLY ISOLATION VALVE WAS REPAIRED IN AUGUST.

THE POND WATER RETURN LINE WAS ALSO REPAIRED DURING THE MONTH.

REPAIRS WERE MADE TO THE ELECTRICAL SYSTEM AFTER A POWER FAILURE IN THE WASTEWATER BUILDING.

9/80	A	43.1	39.2	41.5	39.2				
	В	47.8	47.2	48.2	47.2				
	С	45.6	43.2	45.9	43.2				
	D	46.3	46.0	47.6	46.0				
	SYSTEM	45.6	43.9	45.9	43.9	720	720	316	81.3

## ** PROBLEMS/SOLUTIONS/COMMENTS

MAJOR PROBLEMS DURING SEPTEMBER INCLUDED REPAIR OF THE LIMESTONE BALL MILL. AFTER IT WAS REPAIRED, THE BALL MILL MOTOR BURNED OUT AND HAD TO BE REPLACED.

SLURRY CONTAMINATION OF THE MILL BEARING OIL AND REPAIR OF THE RECYCLE PUMP SUCTION SCREEN CAUSED THE FGD SYSTEM TO BE DOWN FOR SEVERAL HOURS DURING THE MONTH.

10/80	A	73.0	73.0	75.9	73.0				
	В	73.3	65.9	71.8	65.9				
	С	74.2	74.1	75.8	74.1				
	D	73.4	73.2	76.6	73.2				
	SYSTEM	72.8	71.5	75.1	71.6	744	744	532	64.6

## ** PROBLEMS/SOLUTIONS/COMMENTS

DURING OCTOBER THE FGD SYSTEM WAS DOWN APPROXIMATELY 168 HOURS DUE TO PROBLEMS WITH THE LIMESTONE BALL MILL MOTOR.

SOME OUTAGE TIME DURING THE MONTH WAS DUE TO NECESSARY REPAIRS TO THE RECYCLE TANK PUMP AND PROBLEMS WITH THE DISCHARGE VALVE ON THE STORAGE TANK PUMP.

11/80	A	98.9	92.3	100.0	70.3				
	В	96.2	88.1	97.2	67.1				
	С	99.2	91.8	99.6	69.9				
	B	95.4	82.7	100.0	62.9				
	SYSTEM	97.4	88.7	99.2	67.5	720	548	486	50.1

## ** PROBLEMS/SOLUTIONS/COMMENTS

DURING NOVEMBER THE FGD SYSTEM WAS OFF LINE FOR APPROXIMATELY 192 HOURS DUE TO A PLANT OUTAGE (BOILER RELATED).

THE FRESH WATER FLUSH VALVE IN THE MIST ELIMINATOR FAILED ADDING TO THE OUTAGE TIME DURING NOVEMBER.

REPAIRS WERE MADE TO THE RECYCLE TANK SUCTION SCREEN CAUSING SOME OUTAGE TIME.

12/80	A	93.5	92.6	94.1	92.2			
	В	94.9	93.9	95.9	93.5			
	С	87.2	86.0	90.7	85.6			
	D	94.0	93.0	96.0	92.6			
	SYSTEM	92.4	91.4	94.2	91.0	744	741	677 79. <b>7</b>

CENTRAL ILLINOIS LIGHT: DUCK CREEK 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

## ** PROBLEMS/SOLUTIONS/COMMENTS

MINOR PROBLEMS WERE REPORTED FOR DECEMBER, INCLUDING PLUGGING OF RECYCLE TANK PUMP SUCTION SCREENS. REPAIRS WERE MADE DURING THE MONTH TO THE "B" MODULE OUTLET DAMPER AND THE "C" MODULE INLET DAMPER.

1/81	A	92.2	92.1	94.9	92.1
	В	94.9	94.9	97.8	94.8
	С	94.2	94.1	98.0	94.1
	D	88.6	88.6	94.4	88.6
	SYSTEM	92.5	92.4	96.3	92.4

744 744 687 77.9

#### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING JANUARY SOME OUTAGE TIME WAS DUE TO THE PLUGGING OF THE RECYCLE TANK PUMP SUCTION SCREENS.

REPAIRS WERE MADE TO THE INLET DAMPER OF MODULE C AND THE RECYCLE TANK PUMP OF MODULE D DURING THE MONTH.

2/81	A	95.2	95.8	100.0	94.2
	В	80.2	81.5	96.9	80.2
	С	95.1	95.6	100.0	94.0
	D	94.0	94.6	99.8	93.0
	SYSTEM	91.1	91.8	99.2	90.3

672 661 607 59.3

## ** PROBLEMS/SOLUTIONS/COMMENTS

DURING FEBRUARY PROBLEMS WERE ENCOUNTERED THAT NECESSITATED REPAIRS TO THE LIMESTONE CONVEYOR BELT AND THE SLURRY SUPPLY TANK AND LINES.

3/81	A	93.8	88.5	91.6	85.1
	В	82.5	79.9	84.7	76.9
	С	84.7	81.5	85. <b>5</b>	78.4
	D	86.8	84.1	90.8	80.8
	SYSTEM	86.9	83.5	88.2	80.2

744 715 597 68.4

58.6

## ** PROBLEMS/SOLUTIONS/COMMENTS

DURING MARCH OUTAGE TIME WAS DUE TO THE REPLACEMENT OF THE LIMESTONE MILL HIGH LIFT PUMP AND THE SLURRY STORAGE TANK PUMP, BOTH LIMITING THE LIMESTONE SLURRY SUPPLY. THE RECYCLE TANK PUMP ON MODULE C WAS ALSO REPLACED.

ADDITIONAL OUTAGE TIME WAS CAUSED BY PLUGGING IN THE MIST ELIMINATOR SECTION OF ALL THE MODULES.

4/81	A	26.2	27.1	28.1	23.3			
	В	27.1	28.1	29.5	24.2			
	С	44.8	29.1	30.2	25.0			
	D	52.1	28.4	29.5	24.4			
	SYSTEM	37.5	28.1	29.2	24.2	720	619	174

## ** PROBLEMS/SOLUTIONS/COMMENTS

EXTENSIVE PLUGGING THROUGHOUT EACH MODULE WAS OBSERVED AT THE BEGINNING OF AFRIL, RESULTING IN THE NEED FOR EXTENSIVE MAINTENANCE CLEANING, REPAIRS, AND UPGRADING OF EACH MODULE. THE MODULES WERE TAKEN OUT OF SERVICE TWO AT A TIME SO THAT THE WORK COULD BE PERFORMED.

THE ISOLATION DAMPERS ON ALL FOUR MODULES HAVE BEEN A CONTINUAL PROBLEM. THE DAMPERS STICK AND FAIL TO SEAL TIGHTLY RESULTING IN GASEOUS CONDITIONS FOR MAINTENANCE CREWS. THE UTILITY IS PRESENTLY INVESTIGATING THE SITUATION.

ERIOD	MODULE AV	AILABILI	TY OPERABILITY		CE DATA UTILIZATION		. PER	BOILER	FGD	CAP.
5/81	A	68.7	67.0	69.1	65.9					
	В	68.1	66.4 69.9	69.2	65.3					
	С	76.4	69.9	71.4	68.7					
	D	71.4	69.8	73.4	68.5					
	SYSTEM	69.9	68.3	73.4 70.8	67.1		744	731	499	64.0
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			DURING MAY MAJ BILITY DUE TO OPERATION OF T AGE, RESULTED BE PERFORMED W	THE NEED FOR HE MODULE C IN GASEOUS P	R BYPASSING A ISOLATION DA NORKING CONDI	ROUND THE MPER AS WE TIONS SUCH	MODULE.	PROBLI PANSION	IN SME	ΓΗ Γ LEAK-
			PROBLEMS PERSI	ST WITH ALL	THE ISOLATIO	N DAMPERS.				
6/81	1	69.9	60.0	67.4 71.2	51.5					
	В	71.3	63.9	71.2	54.8					
	С	72.4	65.2	70.5 69. <b>5</b>	55.9					
	D	70.3	61.6	69.5	52.9					
	SYSTEM	71.0	62.7	69.6	53.8		720	618	387	52.8
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			DURING JUNE WO DAMPER PROBLEM COULD BE COMPL	IS THE MODULE			_			
7/81	A	78.2	62.4	73.0	53.4					
	В	75.8	62.3	75.7 75.1	53.2					
	С	80.5	64.2	75.1	54.8					
	D	53.6	62.7	75.1	53.6					
	SYSTEM	72.0	62.9	75.1 74.7	53.6 53.8		744	636	400	56.4
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			PROBLEMS WITH AGE DURING THE FOR BYPASSING TENANCE OPERAT	MONTH RESULT FLUE GAS TO	LTED IN LOW S	SYSTEM AVAI	LABILIT'	Y DUE TO	O THE N	4EED
			SIGNIFICANT RE		AS REQUIRED C	OURING THE	монтн он	4 THE M	ODULE A	4,B,
8/81	A	79.4	78.6	80.0	78.6					
	В	79.7	78.9	79.6	78.9					
	С	79.6	78.9	80.3	78.9					
	D	60.3	60.3	62.6	60.3					
	SYSTEM	74.8	74.2	75.6	74.2		744	744	552	75.0
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			ISOLATION DAMP			PROBLEMS CO	DATINUED	TO LOW	ER THE	OVER-
			MIXER REPAIR C	N THE MODULE	E D RECYCLE 1	TANK RESULT	TED IN L	ом мори	LE AVA	IL-
0/81	SYSTEM	.0			.0		744	0	0	.0

32.9 82.6 93.7 26.9 32.9 82.6 93.7 26.9

11/81 A

CENTRAL ILLINOIS LIGHT: DUCK CREEK 1 (CONT.)

			DEDEODMAI	NCE MATA						
PERIOD MODULE					% REN	10VAL	PER		FGD	CAP.
С	32.6	82.1	93.4	26.8						
D	24.5	67.9	81.9	22.2						
SYSTEM	30.7	78.8	90.8	25.7			720	235	185	20.7

## ** PROBLEMS/SOLUTIONS/COMMENTS

A MAJOR UNIT OUTAGE STARTED ON SEPTEMBER 18 AND CONTINUED THROUGH OCTOBER AND ENDED ON NOVEMBER 21. DURING THIS TIME THE SCRUBBER WAS DRAINED OF SLURRY AND CLEANED. ISOLATION DAMPER SEAL AIR PROBLEMS RESULTED IN LOW AVAILABILITY DURING OPERATING PERIODS. IT WAS NECESSARY TO BYPASS THE SYSTEM TO ELIMINATE HAZARDOUS WORKING CONDITIONS DURING MAINTENANCE OPERATIONS.

744

624

511 63.1

70.5

12/81	A	80.3	81.2	81.5	68.1	
	В	81.0	81.6	83.6	68.4	
	С	76.9	81.0	82.5	67.9	
	D	82.1	83.8	84.1	70.3	
	SYSTEM	80.1	81.9	82.9	68.7	

#### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING DECEMBER ISOLATION DAMPER SEAL AIR PROBLEMS RESULTED IN LOW AVAILABILITY DURING OPERATING PERIODS. IT WAS NECESSARY TO BYPASS THE SYSTEM TO ELIMINATE HAZARDOUS WORKING CONDITIONS DURING MAINTENANCE OPERATIONS.

1/82	A	79.1	74.4	76.7	72.4			
	В	73.4	68.6	71.5	66.7			
	С	73.8	69.0	71.0	67.1			
	D	67.3	69.1	71.9	67.3			
	SYSTEM	73.4	70.3	72.8	68.4	744	724	509

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE SCHEDULED BOILER OUTAGE THAT STARTED AT THE END OF DECEMBER ENDED ON JANUARY 4.

THE LOW SYSTEM AVAILABILITY DURING JANUARY WAS PARTIALLY DUE TO THE LIME-STONE IN THE STORAGE PILE BEING FROZEN LIMITING ITS DELIVERY TO THE FGD SYSTEM.

LOW AVAILABILITY WAS ALSO DUE TO ISOLATION DAMPER SEAL AIR PROBLEMS REQUIRING THE NEED FOR BY-PASSING FLUE GAS TO ELIMINATE HAZARDOUS WORKING CONDITIONS DURING MAINTENANCE OPERATIONS.

2/82	A	53.6	53.6	53.6	53.6				
	В	54. <b>5</b>	54 <b>.5</b>	54.5	54.5				
	С	49.3	49.3	49.3	49.3				
	D	55.5	55.5	55.5	55.5				
	SYSTEM	53.2	53.2	53.2	53.2	672	672	358	76.7

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE LOW AVAILABILITY DURING THE MONTH OF FEBRUARY WAS PRIMARILY DUE TO SEVERE PLUGGING OF THE MODULES.

THE ISOLATION DAMPER SEAL AIR PROBLEMS CONTINUED THROUGHOUT FEBRUARY.

3/82	A	32.9	46.6	46.8	32.9				
	В	35.5	50.2	50.4	35.5				
	С	35.7	50.5	50.7	35.7				
	D	34.4	48.7	48.8	34.4				
	SYSTEM	34.6	49.0	49.2	34.6	744	526	258	53.9

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE LOW AVAILABILITY IN MARCH WAS DUE TO SEVERE PLUGGING OF THE ABSORBER MODULES.

MODULE ISOLATION DAMPER SEAL AIR PROBLEMS CONTINUED THROUGH MARCH.

ON MARCH 23 THE UNIT WAS TAKEN OUT OF SERVICE FOR A SCHEDULED OUTAGE. THE UNIT REMAINED OFF-LINE THROUGH THE END OF THE MONTH.

4/82	A	12.2	37.7	46.1	11.0			
	В	19.0	58.9	65.3	15.6			
	С	21.3	66. <b>0</b>	65.6	15.7			
	D	21.3	66.2	65.8	15.8			
	SYSTEM	18.4	57.2	60.7	14.5	720	232	105 17.8

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE SCHEDULED OUTAGE STARTED IN MARCH CONTINUED THROUGH TO APRIL 26. DURING THE OUTAGE THE MODULES WERE CLEANED EXTENSIVELY. THIS HAS SHOWN MUCH IMPROVEMENT IN THE SYSTEM'S RELIABILITY.

5/82	A	91.1	91.1	91.1	91.1				
	В	92.2	92.2	92.2	92.2				
	С	91.9	91.9	91.9	91.9				
	D	91.7	91.7	91.7	91.7				
	SYSTEM	91.7	91.7	91.7	91.7	744	744	682	66.9

## ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE ISOLATION DAMPER SEAL AIR PROBLEMS CONTINUE TO REDUCE THE AVAILABILITY DUE TO THE NEED FOR BY-PASSING FLUE GAS TO ELIMINATE GASEOUS WORKING CONDITIONS DURING MAINTENANCE OPERATIONS.

6/82	A	83.6	83.6	83.6	83.6				
	В	91.6	91.6	91.6	91.6				
	С	91.7	91.7	91.7	91.7				
	D	92.5	92.5	92.5	92.5				
	SYSTEM	89.9	89.9	89.9	89.9	720	720	647 68	3.2

## ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE DOWN TIME DURING JUNE WAS TO REMOVE ANY SCALE ACCUMULATION AND TO CLEAN THE MODULES.

7/82	A	85.5	87.3	89.9	78.3				
	В	88.8	90.6	93.2	81.2				
	С	98.0	79.8	89.6	71.6				
	D	87.3	78.4	89.4	70.3				
	SYSTEM	89.9	84.0	90.5	75.3	744	667	560	57.1

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING JULY.

8/82	A	95.0	95.0	98.5	95.0				
	В	97.4	97.4	98 <b>.3</b>	97.4				
	С	91.6	91. <b>1</b>	96.9	91.1				
	D	96 <b>.5</b>	93.5	97.6	93.5				
	SYSTEM	95.1	94.3	97.8	94.3	744	744	702	69.4

CENTRAL ILLINOIS LIGHT: DUCK CREEK 1 (CONT.)

PERFORMANCE DATA		 	 
PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION			
	SO2 PART.		

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING AUGUST.

9/82	. A	83.3	81.5	95.3	76.6				
	В	88.3	86.5	96.0	81.3				
	С	87.5	86.5	95.9	81.3				
	D	84.7	82.4	99.4	77.5				
	SYSTEM	85.9	84.2	96.6	79.2	72 <b>0</b>	677	570	65.5

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING SEPTEMBER. SYSTEM AVAILABILITY WAS REDUCED ONLY BY BOILER OUTAGE TIME. RELIABILITY MORE ACCURATELY REFLECTS THE OPERATION OF THE SCRUBBER DURING SEPTEMBER.

10/82	A	93.6	93.4	96. <b>0</b>	93.4				
	В	95.9	95.9	96.3	95.9				
	С	95.5	91.5	96.0	91.5				
	D	92.7	92.7	94.6	92.7				
	SYSTEM	94.4	93.4	95.7	93.4	744	744	695	72.2

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMSS WERE ENCOUNTERED DURING OCTOBER.

11/82	A	64.7	85.0	97.4	56.7				
	В	65.5	90.1	97.7	60.1				
	С	65.6	89.5	97.6	59.7				
	D	66.7	90.8	97.8	60.5				
	SYSTEM	65.6	88.9	97.6	59.2	720	480	426	43.8

## ** PROBLEMS/SOLUTIONS/COMMENTS

DURING NOVEMBER THE UNIT WAS DOWN FOR CLEANING AND INSPECTION OF THE MCDULES.

12/82	A	83.0	76.3	88.4	76.3				
	В	87.0	85.7	89.3	85.7				
	С	87.1	87.1	89.8	87.1				
	D	83.8	83.2	89.2	83.2				
	SYSTEM	85.2	83.1	89.2	83.1	744	744	618	63.0

## ** PROBLEMS/SOLUTIONS/COMMENTS

A MAJOR PROBLEM OCCURRED WITH THE LIMESTONE PREPARATION EQUIPMENT FROM DECEMBER 16 TO 23, 1982. THE LIMESTONE BALL MILL MOTOR FAILED AND HAD TO BE EXTENSIVELY REPAIRED. DURING THIS TIME AN EMERGENCY SYSTEM WAS SET UP SO THAT LIMESTONE IN A POWDERED FORM COULD BE CONVEYED TO THE SCRUBBER.

1/83	A	93.1	96.9	99.9	89 <b>.0</b>				
	В	91.9	95.6	99.9	87.9				
	С	93.3	96.1	99.9	88.3				
	D	88.8	92.2	99.9	84.8				
	SYSTEM	91.7	95.2	99.9	87.5	744	684	651	63.8

ERIOD	MODULE AV	AILABILI	TY OPERABILITY	RELIABILITY			PART.	HOURS	HOURS		
	** PROBLE	MS/SOLUT	IONS/COMMENTS								
			THE UTILITY REDURING JANUAR		NO MAJOR FO	GD-RELAT	ED PRO	DBLEMS	WERE EN	NCOUNTE	RED
2/83	٨	61.9	97.2	100.0	61.9						
2/03	B	61.4		100.0	61.4						
	C	62.3		100.0	62.3						
	D	57.4		100.0	57.4						
	SYSTEM	60.7		100.0	60.7			672	428	408	45.7
	** PROBLE	MS/SOLUT	TIONS/COMMENTS								
			THE UNIT WAS	OFF LINE FRO	M FEBRUARY	18 TO 28	3. 198	3 TO R	EPAIR TI	HE EXH	AUST
			STACK.	5.1 E2.1E 1 KG	I EUKUAKI	10 .0 2.	, <b>1</b> ,0.	5 10 K.	M 11	12 27417	
3/83	SYSTEM	.0			.0			744	0	0	.0
	** PROBLE	MS/SOLUT	TIONS/COMMENTS								
			THE UNIT WAS		THE ENTIRE	монтн (	OF MAR	сн то (	IUNITHOC	E REPAI	IRING
4/83	A	.0			.0						
	В	.0			.0						
	С	.0			.0						
	D System	.0			.0			720	0	0	.0
			TIONS/COMMENTS					,,,,	•	·	
	***************************************		THE UNIT WAS	OFF LINE DUR	ING APRIL TO	O CONTI	VUE ST	ACK LIN	NER REP	AIRS.	
5/83	Δ	60.8	85.2	9 <b>9</b> .1	53.5						
5, 05	B	60.1		99.2	59.0						
	Č	60.2		99.1	54.7						
	Ö										
			92.0		57.8						
	SYSTEM	59.7 60.2	92.0 89.6	96.9 98.6	57.8 56.2			744	467	418	40.1
	SYSTEM	59.7 60.2		96.9				744	467	418	40.1
	SYSTEM	59.7 60.2	89.6	96.9 98.6 OUT OF SERVI	56.2 CE UNTIL MA	Y 13, 1	983 DU				
6/83	SYSTEM ** PROBLE	59.7 60.2	89.6 FIONS/COMMENTS THE UNIT WAS	96.9 98.6 OUT OF SERVI	56.2 CE UNTIL MA	Y 13, 1	983 DU				
6/83	SYSTEM ** PROBLE	59.7 60.2 MS/SOLUT 97.3	89.6 FIONS/COMMENTS THE UNIT WAS NANCE ON THE 95.1	96.9 98.6 OUT OF SERVI STACK LINER.	56.2 CE UNTIL MA	Y 13, 1	983 DU				
6/83	SYSTEM  ** PROBLE	59.7 60.2 MS/SOLUT	89.6 FIONS/COMMENTS THE UNIT WAS NANCE ON THE 95.1	96.9 98.6 OUT OF SERVI STACK LINER. 99.3	56.2 CCE UNTIL MA 95.1	Y 13, 1	983 DU				
6/83	SYSTEM  ** PROBLE  A B	59.7 60.2 MS/SOLUT 97.3 99.3	89.6 FIONS/COMMENTS THE UNIT WAS NANCE ON THE 95.1 96.3	96.9 98.6 OUT OF SERVI STACK LINER. 99.3 99.4	56.2 CCE UNTIL MA 95.1 96.3	Y 13, 1	983 DU				
6/83	SYSTEM  ** PROBLE  A B C	59.7 60.2 MS/SOLUT 97.3 99.3 98.5	89.6 FIONS/COMMENTS THE UNIT WAS NANCE ON THE 95.1 96.3 95.2	96.9 98.6 OUT OF SERVI STACK LINER. 99.3 99.4 99.3	56.2 CCE UNTIL MA	Y 13, 1	983 DU		ONTINUE	D MAIN	
6/83	SYSTEM  ** PROBLE  A B C D SYSTEM	59.7 60.2 MS/SOLUT 97.3 99.3 98.5 98.1 98.3	89.6 FIONS/COMMENTS THE UNIT WAS NANCE ON THE 95.1 96.3 95.2 96.6	96.9 98.6 OUT OF SERVI STACK LINER. 99.3 99.4 99.3 98.6	56.2 CCE UNTIL MA 95.1 96.3 95.2 96.6	Y 13, 1	983 DU	E TO C	ONTINUE	D MAIN	ΓΕ-
6/83	SYSTEM  ** PROBLE  A B C D SYSTEM	59.7 60.2 MS/SOLUT 97.3 99.3 98.5 98.1 98.3	89.6 FIONS/COMMENTS THE UNIT WAS NANCE ON THE 95.1 96.3 95.2 96.6 95.8	96.9 98.6 OUT OF SERVI STACK LINER. 99.3 99.4 99.3 98.6 99.1	56.2 CCE UNTIL MA 95.1 96.3 95.2 96.6 95.8			E TO C	ONT INUE	D MAIN	71.0
	** PROBLE  A B C D SYSTEM  ** PROBLE	59.7 60.2 MS/SOLUT 97.3 99.3 98.5 98.1 98.3	89.6 FIONS/COMMENTS THE UNIT WAS NANCE ON THE 95.1 96.3 95.2 96.6 95.8 FIONS/COMMENTS THE UTILITY R	96.9 98.6 OUT OF SERVI STACK LINER. 99.3 99.4 99.3 98.6 99.1	56.2 CCE UNTIL MA 95.1 96.3 95.2 96.6 95.8			E TO C	ONT INUE	D MAIN	71.0
	** PROBLE  A B C D SYSTEM  ** PROBLE	59.7 60.2 MS/SOLUT 97.3 99.3 98.5 98.1 98.3 MS/SOLUT	89.6 FIONS/COMMENTS THE UNIT WAS NANCE ON THE 95.1 96.3 95.2 96.6 95.8 FIONS/COMMENTS THE UTILITY R DURING JUNE.	96.9 98.6 OUT OF SERVI STACK LINER. 99.3 99.4 99.3 98.6 99.1	56.2 CCE UNTIL MA 95.1 96.3 95.2 96.6 95.8			E TO C	ONT INUE	D MAIN	71.0
	** PROBLE  A B C D SYSTEM  ** PROBLE	59.7 60.2 MS/SOLUT 97.3 99.3 98.5 98.1 98.3 MS/SOLUT	89.6 FIONS/COMMENTS THE UNIT WAS NANCE ON THE 95.1 96.3 95.2 96.6 95.8 FIONS/COMMENTS THE UTILITY R DURING JUNE.	96.9 98.6 OUT OF SERVI STACK LINER. 99.3 99.4 99.3 98.6 99.1 EPORTED THAT	56.2  CCE UNTIL MA  95.1 96.3 95.2 96.6 95.8  F NO MAJOR F			E TO C	ONT INUE	D MAIN	71.0
6/83 7/83	** PROBLE  A B C D SYSTEM  ** PROBLE	59.7 60.2 MS/SOLUT 97.3 99.3 98.5 98.1 98.3 MS/SOLUT	89.6 FIONS/COMMENTS THE UNIT WAS NANCE ON THE 95.1 96.3 95.2 96.6 95.8 FIONS/COMMENTS THE UTILITY R DURING JUNE. 98.7 97.7	96.9 98.6 OUT OF SERVI STACK LINER. 99.3 99.4 99.3 98.6 99.1 EPORTED THAT	56.2  CCE UNTIL MA  95.1 96.3 95.2 96.6 95.8  T NO MAJOR F			E TO C	ONT INUE	D MAIN	71.0

8/83 A 100.0 96.4 100.0 96.4

CENTRAL ILLINOIS LIGHT: DUCK CREEK 1 (CONT.)

PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% REI	MOVAL	PER	BOILER HOURS	FGD HOURS	CAP. FACTOR
	В	100.0	94.4	100.0	94.4						
	č	97.8	94.7	100.0	94.7						
	D	100.0	95.3	100.0	95.3						
	SYSTEM	99.5	95.2	100.0 100.0 100.0 100.0	95.2			744	744	708	70.3
9/83	A			100.0							
	В	100.0			94.7						
	Ċ	97.2	92.5	100.0 100.0	92.3						
	D	99.7	95.3	100.0	95.0						
	SYSTEM	97.6	93.0	100.0 100.0	92.8			720	718	668	62.2
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
					NO MAJOR FGD THROUGH SEPT				WERE E	NCOUNTE	ERED
10/87	A	99 9	95.7	100 0	76.8						
10/03	В	99.9 100.0	98.3	100.0	78.9						
	C	100.0	98.2	100.0	78.8						
			97.5	100.0	78.3						
	SYSTEM	100.0	97.4	100.0	78.2			744	597	582	54.6
11/83	٨	97.5	91 0	0.001	81 9						
11/03	B	100.0	91.9	100 0	82 7						
	C	100.0	91.9 94.0	100.0 100.0	84.6						
	Č	100.0	94.0	100.0	84.6						
	D	100.0 98.6	94.0 91.6	100.0 100.0	82.5						
	SYSTEM	99.2	92.5	100.0				72 <b>0</b>	648	600	55.2
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
		т	HE UTTLITY R	FPORTED THAT	THE UNIT WAS	OFF	ITNE E	BUW UC.	TORFP 2	S TO NO	OVEMBER
			, 1983.								
12/83	A	88.5									
	В	88.5	85.2	88.2	85.2						
	С	88.5	85.6	68.2	85.6						
	D			88.3							
	SYSTEM	88.5	85.7	88.2	85.7			744	744	638	69.6
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
		D L	ISABLED THE OADED INTO T	COAL AND LIM HE FACILITY	SEVERE COLD ESTONE HANDLI RESULTING IN WERE CONSIDE	ING EQ THE L	UIPMEN OSS OF	T. LI	MESTONE IMESTON	COULD E SLURI	NOT BE
1/84	A	94.1	89.0	93.5	81.9						
	В	94.3	86.4	93.6	79.4						
	С	94.0	89.2	93.2	82.0						
	D	93.7	87.6	92.7	80.5						
	SYSTEM	94.0	88.0	93.2	80.9			744	684	602	60.2
2/84	A	100.0	96.0	100.0	96.0						
-	В	100.0	96.9	100.0	96.9						
	Č	100.0	98.2	100.0	98.2						
	D	100.0	95.8	100.0	95.8						
	SYSTEM		96.7	100.0	96.7			696	696	673	70.3
3/84	٨	100.0	0( )	100.0	03.7						
J/ 04	A B	100.0	96.1	100.0	91.3						
	C	100.0 97.8	95.1 96.2	100.0	90.4						
	D	100.0	94.2	99.5	89.5 89.1						
	SYSTEM		93.7 94.8	100.0 99.9	90.1			744	707	470	69.1
	5.51211	, , , <u>,</u>	74.0	77.7	70.1			/44	707	6/0	07.1

	MODULE A	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% REMOVAL SO2 PART.				
	** PROBI	LEMS/SOLUTIO	NS/COMMENTS							
				EDODTED THAT	NO MAJOR FGI	n_DELATED DD	OBIEMS	NEDE E	VOEDTEN	JC E D
			URING THE FI			D-KLLXILD FK	00 66113	HERE E	A. EKTE	1CLD
4/84	A	88.9	97.4		86.6					
	В	88.9	90.6	100.0	80.5					
	С	88.9	96.4 89.2	100.0	85.7					
	ם	86.9	89.2	100.0	79.3					
	SYSTEM	88.4	93.4	100.0	83.0		72 <b>0</b>	640	598	58.1
	** PROB	LEMS/SOLUTIO	NS/COMMENTS						ı	
		т	HE UNIT WAS	TAKEN OFF LI	NE ON APRIL	27 FOR INSPE	CTIONS	AND MA	INTENAN	CE.
5/84	A	35.1	84.6	100.0						
	В	32.1	80.2	100.0	26.3					
	С	35.1	84.8	100.0	27.8					
	D	34.1	81.7	100.0	26.8					
	SYSTEM		82.8				744	244	202	14.5
	** PROB	LEMS/SOLUTIO	NS/COMMENTS							
		т	HE UNIT WAS	OFF LINE UNT	TIL MAY 20 DU	E TO INSPECT	MA NOI	THIAM	ENANCE.	•
6/84	A	99.6	95.4		89.5					
	В	99.4	95.3 94.1	99.4	89.4					
	С	99.6	94.1	99.5	88.3					
	D	99.1	94.6	99.5	88.8					
	SYSTEM	99.4	94.8	99.5	89.0		720	676	641	64.4
	** PROB	LEMS/SOLUTIO	NS/COMMENTS							
			HE UTILITY FOR UNSPECIF		THE UNIT WA	S OFF LINE F	ROM JU	4E 15 U	NTIL JU	ME 18
		·	OR UNSPECIF	EU REASONS.						
	_	99.5	98.2	99.9 99.9	97.8					
7/84	A		97.9	99.9	97.5					
7/84	A B	99.5								
7/84		99.5 99.5		99.9	98.0					
7/84	В	99.5 99.5 99.5	97.9 98.4 92.7	99.9 99.9	98.0 92.3					

NO MAJOR FGD-RELATED PROBLEMS WERE REPORTED DURING JULY.

8/84 SYSTEM 744 9/84 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR AUGUST AND SEPTEMBER 1984.

## SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COMPANY NAME PLANT NAME UNIT NUMBER CITY STATE REGULATORY CLASSIFICATION	CENTRAL ILLINOIS PUBLIC SERV NEWTON 1 NEWTON ILLINOIS D 43. ( .100 LB/MMBTU)					
PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW NET UNIT GENERATING CAPACITY W/FGD - MW NET UNIT GENERATING CAPACITY WO/FGD - MW EQUIVALENT SCRUBBED CAPACITY - MW	516. (1.200 LB/MMBTU)  ****** (***** LB/MMBTU)  575  617  575  590  617					
** UNIT DATA - BOILER AND STACK BOILER SUPPLIER BOILER TYPE	COMBUSTION ENGINEERING PULVERIZED COAL BASE					
BOILER SERVICE LOAD  DESIGN BOILER FLUE GAS FLOW - CU.M/S  BOILER FLUE GAS TEMPERATURE - C  STACK HEIGHT M  STACK SHELL	1020.95 (2163480 ACFM) 163.9 (327 F) 162. (530 FT) CONCRETE					
STACK TOP DIAMETER ~ M	***** (**** FT)					
** FUEL DATA FUEL TYPE FUEL GRADE	COAL BITUMINOUS					
AVERAGE HEAT CONTENT - J/G RANGE HEAT CONTENT - BTU/LB AVERAGE ASH CONTENT - % RANGE ASH CONTENT - %	25353. ( 10900 BTU/LB)  ******  12.70  *******					
AVERAGE MOISTURE CONTENT - % RANGE MOISTURE CONTENT - % AVERAGE SULFUR CONTENT - % RANGE SULFUR CONTENT - %	9.50 ***** 3.00 2.8-3.2					
AVERAGE CHLORIDE CONTENT % RANGE CHLORIDE CONTENT %	2.0 *****					
*** PARTICLE CONTROL						
** MECHANICAL COLLECTOR NUMBER TYPE	0 NONE					
** FABRIC FILTER NUMBER TYPE	0 NONE					
** ESP						
NUMBER TYPE SUPPLIER INLET FLUE GAS CAPACITY - CU.M/S	1 COLD SIDE RESEARCH-COTTRELL 1080.7 (2290000 ACFM)					
INLET FLUE GAS TEMPERATURE - C PRESSURE DROP KPA PARTICLE REMOVAL EFFICENCY %	162.8 ( 325 F) .0 ( 0. IN-H20) 99.5					
** PARTICLE SCRUBBER NUMBER GENEPIC TYPE	0 NONE					
SPECIFIC TYPE TRADE NAME/COMMON NAME SHELL GENERIC MATERIAL SHELL SPECIFIC MATERIAL	N/A N/A N/A N/A					
LINER GENERIC MATEPIAL LINER SPECIFIC MATERIAL	N/A N/A					

#### CENTRAL ILLINOIS PUBLIC SERV: NEWTON 1 (CONT.)

## *** FGD SYSTEM

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** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                                THROWAWAY PRODUCT
   SO2 REMOVAL MODE
                                                WET SCRUBBING
                                                DUAL ALKALI
   PROCESS TYPE
   SYSTEM SUPPLIER
                                                GE ENVIRONMENTAL SERVICES
   A-E FIRM
                                                BUELL DIVISION, ENVIROTECH
   DEVELOPMENT LEVEL
                                                FULL SCALE
   NEW/RETROFIT
                                                NEW
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.50
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                   90.00
   ENERGY CONSUMPTION - %
   CURRENT STATUS
                                                 1
   COMMERCIAL START-UP
                                                12/79
   INITIAL START-UP
                                                 9/79
   CONTRACT AWARDED
                                                 8/75
** DESIGN AND OPERATING PARAMETERS
   DESIGN COAL SULFER CONTENT - %
                                                    4.00
** QUENCHER/PRESATURATOR
   NUMBER
   TYPE
                                                PRECOOLER
   CONSTRUCTION MATERIAL GENERIC TYPE
** ABSORBER
   NUMBER
                                                 4
   NUMBER OF SPARES
                                                 Ω
   GENERIC TYPE
                                                PACKED TOWER
    SPECIFIC TYPE
                                                MOBILE BED PACKING
    TRADE NAME/COMMON TYPE
                                                POLYSPHERE SCRUEBER
    SUPPLIER
                                                BUELL DIVISION, ENVIROTECH
   DIMENSIONS - FT
                                                18.0 X 48.0 X 72.0
                                                CARBON STEEL
    SHELL GENERIC MATERIAL
    SHELL SPECIFIC MATERIAL
                                                AISI 1110
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                                N/A
    LINER GENERIC MATERIAL
                                                ORGANIC
    LINER SPECIFIC MATERIAL
                                                GLASS FLAKE-FILLED POLYESTER
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                                NR
   GAS CONTACTING DEVICE TYPE
                                                PLASTIC/RUBBER MOBILE BALLS
   NUMBER OF CONTACTING ZONES
   DISTANCE BETHEEN GAS CONTACTING ZONES - CM
                                                   45.7
                                                                    18.0IN)
                                                               (
                                                               ( 2351 GPM)
    LIQUID RECIRCULATION RATE - LITER/S
                                                  148.
    L/G RATIO - L/CU.M
                                                    1.3
                                                               ( 10.0 GAL/1000 ACF)
    GAS-SIDE PRESSURE DROP - KPA
                                                    1.5
                                                               ( 6.0 IN-H20)
   SUPERFICAL GAS VELOCITY M/SEC SO2 REMOVAL EFFICIENCY - %
                                                    2.5
                                                               ( 8.3 FT/S)
                                                   90.0
** MIST ELIMINATOR
    PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                                PRIMARY COLLECTOR
    NUMBER PER SYSTEM
                                                 8
                                                IMPINGEMENT
    GENERIC TYPE
    SPECIFIC TYPE
                                                BAFFLE
    TRADE NAME/COMMON TYPE
                                                CLOSED VANE
    CONFIGURATION
                                                VERTICAL
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                NR
   CONSTRUCTION MATERIAL SPECIFIC TYPE
** REHEATER
   NUMBER
                                                 1
   GENERIC TYPE
                                                BYPASS
    SPECIFIC TYPE
                                                COLD SIDE
    TRADE NAME/COMMON TYPE
                                                N/A
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                NR
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                NR
** FANS
   NUMBER
   DESIGN
                                                CENTRIFUGAL
```

CENTRAL ILLINOIS PUBLIC SERV: NEWTON 1 (CONT.)

BOOSTER FUNCTION FORCED DRAFT **APPLICATION** DRY SERVICE CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL ** DAMPERS FUNCTION NR NR GENERIC TYPE NR SPECIFIC TYPE CONSTRUCTION MATERIAL GENERIC TYPE NR CONSTRUCTION MATERIAL SPECIFIC TYPE NR LINER GENERIC MATERIAL TYPE NR LINER SPECIFIC MATERIAL TYPE NR ** DUCTWORK SHELL GENERIC MATERIAL TYPE NR SHELL SPECIFIC MATERIAL TYPE NR LINER GENERIC MATERIAL TYPE NR LINER SPECIFIC MATERIAL TYPE NR ** REAGENT PREPARATION EQUIPMENT FUNCTION SLAKER DEVICE NR DEVICE TYPE NR ** REAGENT PREPARATION EQUIPMENT FUNCTION MIX TANK DEVICE N/A DEVICE TYPE AGITATED TANK ** TANKS SERVICE NUMBER NR **** ** PUMPS SERVICE NUMBER **** ** SOLIDS CONCENTRATING/DEWATERING DEVICE VACUUM FILTER NUMBER ** SOLIDS CONCENTRATING/DEWATERING DEVICE THICKENER NUMBER DIMENSIONS - FT 100.0 DIA SHELL GENERIC MATERIAL TYPE INORGANIC SHELL SPECIFIC MATERIAL TYPE HYDRAULICALLY-BONDED CONCRETE ** SOLIDS CONCENTRATING/DEWATERING DEVICE THICKENER NUMBER DIMENSIONS FT 100.0 DIA SHELL GENERIC MATERIAL TYPE CARBON STEEL *** SLUDGE

** TREATMENT

METHOD FIXATION DEVICE PUG MILL PROPRIETARY PROCESS CONVERSION SYSTEMS [POZ-O-TEC]

** DISPOSAL NATURE

FINAL TYPE LANDFILL SITE TREATMENT NR

** WATER BALANCE

WATER LOOP TYPE CLOSED

** FGD SPARE CAPACITY INDICES

ABSORBER - % 33.0

** FGD SPARE COMPONENT INDICES

ABSORBER 1.0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

9/79 SYSTEM 720

#### ** PROBLEMS/SOLUTIONS/COMMENTS

INITIAL OPERATIONS BEGAN AT THIS UNIT ON SEPTEMBER 1 WHEN FLUE GAS WAS PASSED THROUGH THE INDIVIDUAL FGD MODULES FOR TESTING PURPOSES. TESTING OF THE SYSTEM IN AN INTEGRATED MODE IS EXPECTED TO BEGIN IN DECEMBER.

10/79 SYSTEM 744

11/79 SYSTEM 720

#### ** PROBLEMS/SOLUTIONS/COMMENTS

TESTING OPERATIONS CONTINUED THROUGH OCTOBER AND NOVEMBER.

12/79 SYSTEM 75.3 60.1 74.1 59.0 744 730 439

# ** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT BEGAN BURNING HIGH SULFUR COAL ON NOVEMBER 18-19 AT WHICH TIME THE FGD SYSTEM BEGAN OPERATIONS IN AN INTEGRATED MODE FOR THE FIRST TIME.

INITIAL START UP PROBLEMS HAVE INCLUDED MIST ELIMINATOR PLUGGING.

LINING FAILURES HAVE ALSO BEEN ENCOUNTERED DURING START UP PHASE.

THE UNIT PASSED A COMPLIANCE TEST ON DECEMBER 5, 1979. IT WAS DETERMINED THAT THE FGD SYSTEM CONTROLLED SO2 EMISSIONS TO WELL BELOW THE ALLOHABLE 1.2 LB/MM BTU STANDARD.

1/80	A	68.3	57.1	63.5	55.5			
	В	66.4	60.6	64.9	58.9			
	С	52.2	48.8	60.5	47.4			
	ס	21.0	19.1	26.3	18.5			
	SYSTEM	52.0	46.4	53.8	45.1	744	723	336

#### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING JANUARY TESTS WERE CONDUCTED TO CERTIFY THE GAS EMISSIONS MONITOR AT NEWTON.

PRESATURATOR CORROSION AND EXPANSION JOINT REPAIRS AND A DEPLETION OF THE FLYASH USED FOR SLUDGE STABILIZATION ACCOUNTED FOR THE LOW JANUARY DEPENDABILITY FIGURES.

2/80	A	61.1	42.4	45.0	42.4			
	В	74.4	55.7	57.7	55.7			
	С	78.2	58.5	59.1	58.5			
	D	.0	.0	. 0	.0			
	SYSTEM	53.4	39.2	40.4	39.2	696	696	273

UTILITY FGD SURVEY: OCTOBER 1983 - SEPTEMBER 1984

CENTRAL ILLINOIS PUBLIC SERV: NEWTON 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

#### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING FEBRUARY THE D-MODULE WAS UNAVAILABLE DUE TO THE COLLAPSE OF THE PRECOOLER MIST ELIMINATORS CAUSED BY A TEMPERATURE EXCURSION.

REPAIR WORK ON THE PRESATURATOR CORROSION AND EXPANSION JOINTS AS WELL AS THE FLYASH DEPLETION PROBLEM CONTINUED TO YIELD LOW DEPENDABILITY FIGURES FOR FEBRUARY.

3/80	A	53.4	52.6	53.1	52.3		
	В	47.0	42.3	48.0	42.1		
	С	44.5	41.1	46.5	41.0		
	D	.0	. 0	.0	.0		
	SYSTEM	36.2	34.0	36.9	33.9	744	740

#### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE FIRST QUARTER, 1980, THE FOLLOWING PROBLEMS WERE ENCOUNTERED:

252

THE VALVES AND PIPING IN THE PRECOOLER LOOP EXPERIENCED CORROSION.

THE MIST ELIMINATOR ON THE D MODULE FAILED.

THE FLY ASH SUPPLIES DEPLETED.

RUBBER LINING AND DUCTWORK LINING FAILURES OCCURRED.

BOOSTER FAN EXPANSION JOINT FAILURE OCCURRED.

THE THICKENER EXPERIENCED PLUGGING.

THESE COMBINED PROBLEMS ACCOUNTED FOR THE LOW MARCH PERFORMANCE FIGURES. FOR THE QUARTER, THE TOTAL SYSTEM WAS AVAILABLE 47.2% AND WAS UTILIZED 39.4% OF THE TIME.

4/80	A	33.8	31.3	31.4	31.3			
	В	35.4	25.8	25.8	25.8			
	С	37.4	35.6	35.6	35.6			
	D	26.1	21.8	21.8	21.8			
	SYSTEM	33.2	28.6	28.6	28.6	720	720	206

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE NEWTON 1 FGD SYSTEM WAS OUT OF SERVICE DURING THE FIRST 12 DAYS OF APRIL FOR NECESSARY REPAIRS ON THE OUTLET DUCT LININGS. THE UTILITY INDICATED THAT THE LINING FAILURES MAY HAVE RESULTED FROM IMPROPER APPLICATION.

DURING THE LAST 18 DAYS OF APRIL MINOR PROBLEMS WERE EXPERIENCED WITH THE OCCURANCE OF PLUGGING IN THE SODIUM CARBONATE THICKENER AND CORROSION OF THE VALVES IN THE PRESATURATOR CIRCUIT.

<b>5/80</b>	A	.0	. 0	. 0	.0				
	В	9.7	9.6	9.6	6.2				
	С	9.7	9.6	9.6	6.2				
	D	.0	.0	.0	. 0				
	SYSTEM	4.8	4.8	4.8	3.1	744	477	23 45.5	5

# ** PROBLEMS/SOLUTIONS/COMMENTS

DURING MAY, THE FGD SYSTEM WAS DOWN BECAUSE THE FLUIDIZING STONES WERE CAKED WITH FLY ASH. THIS WAS CAUSED BY IMPROPER WIRING OF THE HEATER WHICH BLOWS OVER THE STONES. THE HEATER WAS REWIRED AND THE FLUIDIZING STONES REPLACED. FLUIDIZING STONES ARE LOCATED IN THE FLYASH SILO. HEATED AIR PASSES THROUGH THESE POROUS STONES TO AERATE OR "FLUIDIZE" THE FLYASH SO THAT IT CAN BE CONVEYED TO THE FLYASH/SLUDGE MIXER. WHEN THE FLYASH SUPPLY IS DEPLETED OR THE MATERIAL CANNOT BE DELIVERED TO THE MIXER THE SCRUBBING SYSTEM IS SHUT DOWN. THE SLUDGE MUST BE TREATED WITH FLYASH BEFORE DISPOSAL.

6/80 A .0 .0 .0 .0

			PERFORMA!	NCE DATA						
	AVAILABILITY				% RE	MOVAL	PER	BOILER HOURS	FGD	CAP.
В	40.3	40.3	40.3	40.3						
С	40.4	40.4	40.4	40.4						
D	.0	.0	. 0	.0						
SYSTEM	20.2	20.2	20.2	20.2			720	720	145	63.0

#### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING JUNE THE A AND D MODULES WERE UNAVAILABLE FOR OPERATION BECAUSE THE MIST ELIMINATORS COLLAPSED.

THE SYSTEM WAS SHUTDOWN DURING THE FIRST HALF OF THE MONTH TO REPAIR THE DRY FLYASH COLLECTION SYSTEM WHICH ACCOUNTED FOR THE LOW B AND C MODULE FIGURES.

7/80	A	3.5	3.7	3.7	3.5			
	В	3.6	3.9	3.9	3.6			
	С	.0	.0	.0	.0			
	D	.0	.0	. 0	.0			
	SYSTEM	1.8	1.9	1.9	1.8	744	698	13 67.8

#### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING JULY PROBLEMS WERE ENCOUNTERED WITH THE MIST ELIMINATORS.

SOME OF THE SYSTEM OUTAGE TIME RESULTED FROM REPAIRS MADE NECESSARY BY THE OCCURRENCE OF CORROSION IN THE PRESATURATOR.

SCRUBBER PLUGGING DURING JULY CONTRIBUTED TO THE LOW FGD SYSTEM  $_$  AVAILABILITY.

8/80	A	.0	. 0	. 0	.0				
	В	64.7	50.2	50.2	49.3				
	С	51.2	34.1	36.9	33.5				
	D	37.6	21.9	24.0	21.5				
	SYSTEM	53.8	36.4	39.9	35.8	744	731	266	68.2

#### ** PROBLEMS/SOLUTIONS/COMMENTS

PLUGGING PROBLEMS WITHIN THE FGD SYSTEM WERE THE CAUSE OF DOWN TIME IN AUGUST.

BECAUSE OF CHANGES IN SYSTEM OPERATIONS, ONLY 3 MODULES ARE NEEDED TO MEET CURRENT SO2 REGULATIONS.

9/80	A	69.0	20.3	48.6	10.0				
	В	99.6	74.6	80.3	36.8				
	С	96.9	35.8	66.8	17.6				
	D	99.6	80.8	80.8	39.9				
	SYSTEM	99.1	67.8	82.5	33.4	720	355	241	33.2

# ** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER WAS TAKEN OUT OF SERVICE ON SEPTEMBER 16, 1980 FOR A SCHEDULED MAINTENANCE OUTAGE.

10/80	A	75.9	38.5	46.3	16.9			
	В	83.7	47.9	56.5	21.1			
	С	81.0	51.6	54.5	22.7			
	D	62.4	7.0	13.7	3.1			
	SYSTEM	81.5	48.4	46.3	21.3	744	328	119 30.4

UTILITY FGD SURVEY: OCTOBER 1983 - SEPTEMBER 1984

CENTRAL ILLINOIS PUBLIC SERV: NEWTON 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

#### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING OCTOBER THE FGD SYSTEM AVAILABILITY WAS LOW AS A RESULT OF LOW LIQUOR TEMPERATURES IN THE SCRUEBER FOLLOWING THE FOUR WEEK BOILER OUTAGE. THE LIQUOR WAS PREHEATED WITH STEAM TO PREVENT PLUGGING DUE TO THE "SALTING OUT" OF REAGENTS AT LOW TEMPERATURES.

11/80	A B C	93.6 79.6 89.4	69.9 59.9 58.8	98.2 100.0 97.2	69.9 59.9 58.8				
	D	79.6	70.1	99.0	70. <b>0</b>				
	SYSTEM	99.3	84.9	100.0	84.8	72 <b>0</b>	719	465	69.6

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR OUTAGES OCCURRED DURING NOVEMBER.

12/80	A	64.5	45.9	63.8	45.7			
	В	71.5	68.7	72.2	68.4			
	С	72.7	42.1	63.4	41.9			
	D	71.5	52.8	66.7	52.6			
	SYSTEM	74.1	69.5	84.8	69.3	744	741	70.7

# ** PROBLEMS/SOLUTIONS/COMMENTS

FGD SYSTEM AVAILABILITY WAS LOWERED DURING DECEMBER AS A RESULT OF THICKENER PLUGGING PROBLEMS.

1/81	A	90.5	75.0	99.1	75.0				
	В	73.9	58.1	99.5	58.1				
	С	96.2	79.8	100.0	79.8				
	D	88.3	57.1	100.0	57.1				
	SYSTEM	99.1	89.5	100.0	89.5	744	744	425	71.4
2/81	A	93.2	49.8	100.0	49.7				
	В	96.0	81.1	100.0	81.0				
	С	92.3	72.3	100.0	72.2				
	D	100.0	82.4	100.0	82.3				
	SYSTEM	100.0	95.1	100.0	94.9	672	671	639	66.6
3/81	A	94.1	56.9	100.0	52.7				
	В	87.1	80.6	100.0	75.0				
	С	86.4	65.9	100.0	61.0				
	D	94.1	65.5	100.0	60.6				
	SYSTEM	90.4	67.2	100.0	62.2	744	689	463	63.3

^{**} PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE FIRST QUARTER 1981.

4/81	A B C D	96.1 98.2 96.1 93.6	73.3 82.8 60.6 85.1	100.0 100.0 100.0 100.0	73.3 82.8 60.6 85.1				
	SYSTEM	99.9	94.5	100.0	94.5	720	720	680	73.2

# ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING APRIL.

5/81 A 93.3 66.	9 98.3	61.4
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PERIOD	MODULE	AVAILABILITY			UTILIZATION	% REI SO2	MOVAL	PER	BOILER		CAP.
	В	85.3	78.0	98.5	71.6						
	С	91.9	76.6	98 <b>.5</b>	70.3						
	D	93.4	43.2	97.4	39.7						
	SYSTEM	100.0	88.3	98.4	81.0			744	683	603	60.5
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			HE UTILITY RI URING MAY.	EPORTED THAT	NO MAJOR FG	D-RELA	TED PR	OBLEMS	WERE E	NCOUNTE	ERED
6/81	A	96.5	64.9	100.0 100.0	64.6 71.7						
	В	92.2	72.1	100.0	71.7						
	С	88.3	1.1 /.	100.0 100.0	46.1						
	D	96.7	92.2	100.0	91.7						
	SYSTEM	100.0	91.9	100.0	91.3			720	716	658	64.3
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
		D	URING JUNE N	O MAJOR FGD-	RELATED PROB	LEMS W	ERE EN	COUNTER	RED.		
7/81	A	79.6	44.5	79.2	42.9						
	В	85.3	64.6	84.8	62.2						
	С	84.5	35.0	74.3	33.7						
	D	82.5	68 2	84.9	65.7						
	SYSTEM	89.2	70.2	98.9	67.6			744	717	503	55.4
8/81	A	92.7	55.6	100.0	55.6						
	В	90.5	64.5	100.0	64.5						
	С	100.0	64.5 67.1	100.0 100.0	67.1						
	D			100.0	57.0						
	SYSTEM	100.0	81.6	100.0	81.6			744	744	607	57.9
9/81	A	88.8	45.3	100.0	38.9						
	В	99.0	78.4	100.0	67.4						
	С	100.0	79.5	100.0 100.0	68.3						
	D	97.9	38.8	100.0	33.3						
	SYSTEM	100.0	80.7					720	619	499	47.2
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			SCHEDULED M EPTEMBER 26.		UTAGE (BOTH	BOILER	AND F	GD SYS	TEM) BE	GAN ON	
10/81	SYSTEM	100.0	.0	.0	.0			744	7	0	.1
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			URING OCTOBE	R A SCHEDULE	D MAINTENANC	E OUTA	GE OF	THE GEI	NERATIN	G UNIT	
11/81	A	98.6	63.9	76.2	63.5						
	В	85.8	27.8	63.0	27.6						
	С	97.5	55.5	73.0	55.1						
	D	85.7	61.3	73.1	60.8						
	SYSTEM		69.5	95.1	68.7			720	715	497	61.1
12/81	A	94.8	55.8	99.8	53.8						
	В	84.8	42.2	100.0	40.7						
	Č	100.0	82.0	100.0	79.0						
	D	100.0	73.5	100.0	70.8						
	SYSTEM		84.5	100.0	81.4			744	717	612	52.6
	3.31011	230.0	- 12		U4.7			, , ,		912	20.0

ERIOD	MODULE A	/AILABILI	TY OPERABILITY	RELIABILITY	UTILIZATION	% REMOVAL SO2 PART.	PER HOURS	BOILER HOURS	FGD HOURS	CAP. FACTO
	** PROBLE	EMS/SOLUT	IONS/COMMENTS							
			DURING NOVEMB PROBLEMS WERE			TY REPORTED	THAT	OLAM ON	R FGD-8	RELATE
1/82	A	100.0	58.5	100.0	58.2					
	В	100.0	97.9	100.0	97.4					
	С	50.5	42.3 79.6	100.0	42.1					
	ם	93.4	79.6	100.0	79.3					
	SYSTEM	100.0	92.7	100.0	92.3		744	740	687	63.5
2/82	A	90.0	37.2	100.0	37.2					
	В	93.8	37.2 79.6	100.0	79.6					
	Ċ	100.0	92.1	100.0	92.1					
	ם	91.1	82.0	100.0	82.0					
	SYSTEM	100.0	82. <b>0</b> 97. <b>0</b>	100.0	97.0		672	672	6 <b>5</b> 2	70.1
1/82	A	an a	40.1	84 2	40 1					
,, 00	Ê	93.1	91 4	92 4	91.4					
	č	80.8	61.7	92.4 90.0	61.7					
	D	90.5								
	SYSTEM		85.2	89.1 100.0	85.2		744	744	634	66.4
	** PROBLE	EMS/SOLUT	IONS/COMMENTS							
			THE UTILITY R			-RELATED PRO	BLEMS	WERE EN	COUNTE	RED
			DURING THE FIR	RST QUARTER 1	982.	•				
<del>1</del> /82	A	100.0	60.9	100.0	46.5					
	В	98.2	78.9	100.0 100.0	60.3					
	С	94.9	91.7	100.0 100.0	70.0					
	ם	95.0	23.5	100.0	17.9					
	SYSTEM	100.0	85.0	100.0	64.9		720	550	467	43.3
/82	A	71.0	.0		. 0					
	8	100.0	.0 94.3	100.0	26.5					
	С	100.0	40.7	100.0	11.4					
	D	99.3		100.0	26.9					
	SYSTEM	100.0	76.9		21.6		744	209	161	13.1
/82	Δ	. 0	.0		.0					
	В	99.7		100.0	97.5					
	Ċ	100.0	62.7		62.6					
	D	98.3	52.6	100.0	52.5					
	SYSTEM	99.4	71.0	100.0	70.9		720	719	510	<b>3</b> 8.2
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			THE UTILITY REDURING THE SEC	EPORTED THAT	NO MAJOR FGD	-RELATED PRO	BLEMS	WERE EN	1COUNTE	RED
7/82	Δ	22.3	14.0	92.9	17.0					
	B	86.6	79.8	92.8 98.8	13.8					
	Ċ	94.1	50.0	97.4	79.0 4 <b>9</b> .5					
	D	98.9	81.1	98.7	80.2					
	SYSTEM	97.8	75.2	100.0	74.4		744	737	553	45.5
3/82	A	98.5	97.8	99.5	97.8					
	B	.0	.0	77.2	.0					
	Ċ	98. <b>9</b>	76.2	100.0	76.2					
	D	100.0	48.4	100.0	48.4					
	SYSTEM	99 1	74.2	100.0	76.4					

99.8

74.2

744 744

522 43.7

74.2

SYSTEM

99.1

		AVATI ARTI TTV									
PERIOD	MODULE	AVAILABILITY				<b>S</b> 02	PART.	HOURS	HOURS	HOURS	FACTOR
9/82	A B	100.0 .0 100.0 100.0	78.7 0	100.0	76.4 n						
		100.0	70 B	100 0	68.8						
	C D	100.0	70.0	100.0	40.0						
	CVETEM	100.0	71.6	100.0	71.6			720	699	<b>51</b> /4	63 6
					/1.4			720	677	514	41.6
	** PRO	BLEMS/SOL <b>UTI</b> O	NS/COMMENTS								
			HE UTILITY R URING THE TH			GD-RELAT	red PR	OBLEMS	WERE EI	NCOUNTE	ERED
10/82	A	48.3	45.7	90.8	45.2						
	В	48.4	35.5	96.0	35.1						
	С	96.5	58.8	94.3	58.2						
	D	93.3	87.8	96.1	86.8						
	SYSTEM	48.4 96.5 93.3 95.5	75.9	100.0	75.1			744	736	559	50.6
11/82	A B	.0	.0 88.0 42.1 89.9		.0						
	В	92.4	88. <b>0</b>	97.9	76.3						
	C	95.4	42.1	95.3	36.5						
	Ď	97.1	89.9	97.7	77.9						
	SYSTEM	96.8	73.3	97.4	63.6			72 <b>0</b>	624	458	38.9
12/82	A	51.1	35.1 70.8 45.4 63.1	91.7	23.8						
	В	94.6	70.8	96.0	48.0						
	C D	91.1	45.4	94.2	30.8						
	D	74.6	63.1	96.4	42.7						.5
	SYSTEM	93.3	73.4	100.0	49.7			744	504	370	30.5
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			HE UTILITY RURING THE FO			GD-RELAT	TED PR	OBLEMS	WERE E	NCOUNTE	ERED
1/83	A	77.3	28.0 134.7	100.0	19.0						
	В	100.0	134.7	100.0	91.3						
	С	99.3	39. <b>3</b>	88.8	26.6						
	D	88.3	39. <b>3</b> 12 <b>1</b> .6	100.0	82.4						
	_	100.0	77.5	100.0	73.1			744	504	544	48.0
2/83	A	99.6	70.5 36.0	100.0	70.5						
	В	41.8	36.0	99.2	36.0						
	С	100.0	18.2	100.0	18.2						
	D	100.0	100.0	100.0	100.0						
	SYSTEM	99.9	74.3	100.0	74.3			672	672	500	54.4
3/83	A	81.7	56.9	100.0	56.9						
	В	94.4	94.1	99.7	94.1						
	С	19.4	3.0	100.0	3.0						
	D	94.1	94.1	100.0	94.1						
	SYSTEM	97.6	81.5	99.7	81.5			744	744	606	64.4
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			HE UTILITY R URING THE FI			GD-RELA	TED PR	OBLEMS	WERE E	NCOUNT	ERED
4/83	A	99.4	95.6	100.0	95.6						
	В	97.8	89.3	100.0	89.3						
	c	.0	. 0		.0						
	D	93.3	88.9	100.0	88.9						
	SYSTEM		91.3	100.0	100.0			720	720	720	76.8
	J. J. L.	,	, =		200.0				, 20	, 20	

	MODULE	AVAILABILI	TY OPERABILITY	RELIABILITY	_	% REMOVAL SO2 PART.	PER			CAP.
	** PROE	BLEMS/SOLUT	TIONS/COMMENTS							
			MODULE C WAS (	OUT OF SERVI	CE DURING TH	E ENTIRE MONT	TH OF A	APRIL FO	OR LINI	NG
5/83	A	100.0		100.0	1.3					
	В	100.0	50.0	100.0 100.0	.7					
	С	.0	.0		.0					
	D		100.0		1.3					
	SYSTEM	100.0	83.5	100.0	1.1		744	10	8	. 6
	** PROE	BLEMS/SOLUT	TIONS/COMMENTS							
			THE UNIT WAS FOUTAGE.	REMOVED FROM	SERVICE ON	MAY 1 FOR AN	ANNUAL	MAINTE	NANCE	
			MODULE C REMAIL	INED OUT OF	SERVICE DURI	NG MAY FOR RE	PAIR C	OF THE F	LAKEGL	ASS
6/83	A	99 9	77 9	99 7	45.0					
J, 03	B	100.0	77.9 71.2	99.7 100.0	45.0					
	Ċ			100.0						
	ם	.0	. 0		. 0					
	SYSTEM	99.9	76.2	100.0	44.0		720	416	317	43.1
	** PROE	BLEMS/SOLUT	TIONS/COMMENTS							
			THE UNIT REMAI	THED OUT OF	EDVICE HINTT			E. M. IAITAI		
			OUTAGE.		DERVICE ONII	L JUNE 15 FOR	THE A	INNUAL I	IATHIEN	ANCE
7/83	A	100.0	OUTAGE.  MODULE D WAS C	OUT OF SERVIC						
7/83	<b>A</b> B	100.0 98.9	OUTAGE.  MODULE D WAS 0	OUT OF SERVIC	CE ALL MONTH					
7/83	B C		OUTAGE.  MODULE D WAS C  93.3  98.9	DUT OF SERVIC 100.0 100.0	CE ALL MONTH					
7/83	B C D	98.9 100.0	OUTAGE.  MODULE D WAS 0  93.3  98.9  100.0	100.0 100.0 100.0 100.0	93.3 98.9 100.0					
7/83	B C	98.9 100.0	OUTAGE.  MODULE D WAS C  93.3  98.9  100.0	100.0 100.0 100.0 100.0	93.3 98.9 100.0	FOR REPAIR C		FLAKEGL		
7/83	B C D SYSTEM	98.9 100.0 .0 99.6	OUTAGE.  MODULE D WAS 0  93.3  98.9  100.0	100.0 100.0 100.0 100.0	93.3 98.9 100.0	FOR REPAIR C	F THE	FLAKEGL	ASS LI	
7/83	B C D SYSTEM	98.9 100.0 .0 99.6	OUTAGE.  MODULE D WAS 0  93.3  98.9  100.0  .0  97.4	100.0 100.0 100.0 100.0 100.0	93.3 98.9 100.0 .0 97.4	FOR REPAIR C	744	FLAKEGL 744	ASS LI 725	NING.
7/83 3/83	B C D SYSTEM	98.9 100.0 .0 99.6	OUTAGE.  MODULE D WAS 0  93.3  98.9  100.0  .0  97.4  TIONS/COMMENTS  MODULE D WAS 0	100.0 100.0 100.0 100.0 100.0	93.3 98.9 100.0 .0 97.4	FOR REPAIR C	744	FLAKEGL 744	ASS LI 725	NING.
	B C D SYSTEM ** PROB	98.9 100.0 .0 99.6 SLEMS/SOLUT	OUTAGE.  MODULE D WAS 0  93.3  98.9  100.0  .0  97.4  TIONS/COMMENTS  MODULE D WAS 0 LINING REPAIRS	100.0 100.0 100.0 100.0 100.0	93.3 98.9 100.0 .0 97.4 E DURING TH	FOR REPAIR C	744	FLAKEGL 744	ASS LI 725	NING.
	B C D SYSTEM ** PROB	98.9 100.0 .0 99.6 SLEMS/SOLUT 100.0 94.6 100.0	OUTAGE.  MODULE D WAS 0 93.3 98.9 100.0 .0 97.4  TIONS/COMMENTS  MODULE D WAS 0 LINING REPAIRS	100.0 100.0 100.0 100.0 100.0	93.3 98.9 100.0 .0 97.4	FOR REPAIR C	744	FLAKEGL 744	ASS LI 725	NING.
	B C D SYSTEM ** PROB	98.9 100.0 .0 99.6 SLEMS/SOLUT 100.0 94.6 100.0 16.8	OUTAGE.  MODULE D WAS COMMENTS  MODULE D WAS COMMENTS  MODULE D WAS COMMENTS  87.0 82.9	100.0 100.0 100.0 100.0 100.0	93.3 98.9 100.0 .0 97.4 CE DURING THE	FOR REPAIR C	744	FLAKEGL 744	ASS LI 725	NING.
	B C D SYSTEM ** PROB	98.9 100.0 .0 99.6 SLEMS/SOLUT 100.0 94.6 100.0	OUTAGE.  MODULE D WAS COMMENTS  MODULE D WAS COMMENTS  MODULE D WAS COMMENTS  87.0 82.9 99.6	100.0 100.0 100.0 100.0 100.0	93.3 98.9 100.0 .0 97.4 EE DURING THE 87.0 82.9 99.6	FOR REPAIR C	744	FLAKEGL 744	ASS LI 725	NING.
	B C D SYSTEM ** PROB	98.9 100.0 .0 99.6 BLEMS/SOLUT 100.0 94.6 100.0 16.8 100.0	OUTAGE.  MODULE D WAS COMMENTS  MODULE D WAS COMMENTS  MODULE D WAS COMMENTS  87.0 82.9 99.6 15.1	100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0	93.3 98.9 100.0 .0 97.4 EE DURING THE 87.0 82.9 99.6 15.1	FOR REPAIR C	744 745 740F J	FLAKEGL 744 JULY FOR	725	NING.
	B C D SYSTEM ** PROB	98.9 100.0 .0 99.6 BLEMS/SOLUT 100.0 94.6 100.0 16.8 100.0	OUTAGE.  MODULE D WAS 0 93.3 98.9 100.0 .0 97.4  TIONS/COMMENTS  MODULE D WAS 0 LINING REPAIRS 87.0 82.9 99.6 15.1 94.8	100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0	93.3 98.9 100.0 .0 97.4 CE DURING THE 87.0 82.9 99.6 15.1 94.8	FOR REPAIR O	744 H OF J	FLAKEGL 744 JULY FOR	725	NING.
	B C D SYSTEM ** PROB	98.9 100.0 .0 99.6 BLEMS/SOLUT 100.0 94.6 100.0 16.8 100.0	OUTAGE.  MODULE D WAS COMMENTS  MODULE D WAS COMMENTS  MODULE D WAS COMMENTS  87.0 82.9 99.6 15.1 94.8	100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0	93.3 98.9 100.0 .0 97.4 CE DURING THE 87.0 82.9 99.6 15.1 94.8	FOR REPAIR O	744 H OF J	FLAKEGL 744 JULY FOR	725	NING.
3/83	B C D SYSTEM ** PROB A B C D SYSTEM ** PROB	98.9 100.0 .0 99.6 SLEMS/SOLUT 100.0 94.6 100.0 16.8 100.0	OUTAGE.  MODULE D WAS COMMENTS  MODULE D WAS COMMENTS  MODULE D WAS COMMENTS  87.0 82.9 99.6 15.1 94.8  MODULE D WAS COMMENTS  ABSORBER LINER	100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0	93.3 98.9 100.0 .0 97.4 CE DURING THE 87.0 82.9 99.6 15.1 94.8	FOR REPAIR O	744 H OF J	FLAKEGL 744 JULY FOR	725	NING.
3/83	B C D SYSTEM ** PROB A B C D SYSTEM ** PROB	98.9 100.0 .0 99.6 SLEMS/SOLUT 100.0 94.6 100.0 16.8 100.0	OUTAGE.  MODULE D WAS COMMENTS  MODULE D WAS COMMENTS  MODULE D WAS COMMENTS  87.0 82.9 99.6 15.1 94.8  MODULE D WAS COMMENTS  ABSORBER LINER	100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0	93.3 98.9 100.0 .0 97.4 CE DURING THE 87.0 82.9 99.6 15.1 94.8	FOR REPAIR O	744 H OF J	FLAKEGL 744 JULY FOR	725	NING.
3/83	B C D SYSTEM ** PROB A B C D SYSTEM ** PROB	98.9 100.0 .0 99.6 SLEMS/SOLUT 100.0 94.6 100.0 16.8 100.0 SLEMS/SOLUT	OUTAGE.  MODULE D WAS COMMENTS  MODULE D WAS COMMENTS  MODULE D WAS COMMENTS  87.0 82.9 99.6 15.1 94.8  TONS/COMMENTS  ABSORBER LINER  56.7 32.8	100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0 100.0	93.3 98.9 100.0 .0 97.4 SE DURING THE 87.0 82.9 99.6 15.1 94.8 MODULE D COM	FOR REPAIR O	744 H OF J	FLAKEGL 744 JULY FOR	725	NING.

536

.0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

#### ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE A WAS UNAVAILABLE DURING PART OF SEPTEMBER DUE TO REPAIR OF THE ABSORBER'S FLAKEGLASS LINING.

MODULE B WAS UNAVAILABLE DURING PART OF SEPTEMBER DUE TO SCALE AND TRASH BUILD UP IN THE RECIRCULATION PUMP SUCTION STRAINERS CAUSING PLUGGING PROB-

10/83	A	82.3	57.8	100.0	57.8		
	В	61.3	31.9	100.0	31.9		
	С	100.0	68.8	100.0	68.8		
	D	84.7	57.8	100.0	57.8		
	SYSTEM	100.0	72.1	100.0	72.1	744	744

#### ** PROBLEMS/SOLUTIONS/COMMENTS

MODULES A AND D WERE DOWN DURING PART OF OCTOBER DUE TO DUCTWORK LINING REPAIRS.

MODULE B WAS OUT OF SERVICE DURING PART OF THE MONTH DUE TO PUMP PACKING SLEEVE FAILURE.

11/83	A	100.0	99.8	100.0	85.0				
	В	10.6	. 0		.0				
	С	98.9	98.4	100.0	83.8				
	ס	100.0	96.7	100.0	82.4				
	SYSTEM	100.0	98.3	100.0	83.7	720	613	603	.0

## ** PROBLEMS/SOLUTIONS/COMMENTS

# MODULE B WAS DOWN DURING NOVEMBER DUE TO RECIRCULATING PUMP FAILURE.

12/83	A	80.6	67.3	100.0	57.9				
	В	93.5	88.4	99.1	76.1				
	ε	91.9	57.3	95.1	49.3				
	D	98.1	89.5	99.5	77.0				
	SYSTEM	100.0	100.0	100.0	86.8	744	640	646	.0

# ** PROBLEMS/SOLUTIONS/COMMENTS

A UNIT OUTAGE OCCURRED FROM DECEMBER 1 TO DECEMBER 5, 1983.

1/84	A	98.1	93.1	99.9	93.1			
	В	61.3	41.0	99.7	41.0			
	С	93.1	49.7	99.7	49.7			
	D	99.9	89.9	99.9	89.9			
	SYSTEM	100.0	91.3	100.0	91.3	744	744	679

# ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING JANUARY.

2/84	A	59.5	12.0	100.0	10.2			
	В	92.8	97. <del>6</del>	100.0	83.2			
	С	92.7	84.5	100.0	72.0			
	ם	88.8	52.4	100.0	44.7			
	SYSTEM	100.0	82.2	100.0	70.0	696	593	487

RIO	MODULE A	VAILABILI	TY OPERABILITY		Y UTILIZATION	SO2 PART.	HOURS	HOURS	HOURS	
	** PROBL	EMS/SOLUT	IONS/COMMENTS							
			MODULE A WAS	UNAVAILABLE	DURING PART	OF FEBRUARY	DUE TO	A PLUG	GED SPR	YAY
/84	A	89. <b>0</b>	9.9	100.0						
	В	100.0	98. <b>5</b> 99.2	100.0	95.0					
	С	100.0	99.2	100.0	95.7					
	D	89.7	51.6	100.0	49.7					
	SYSTEM	100.0			83.3		744	718	620	
	** PROBLI	EMS/SOLUT	IONS/COMMENTS							
			THE UTILITY R		T NO MAJOR FGI	O-RELATED PR	OBLEMS	WERE EN	COUNTE	RED
/84	A	81.1	55.6	100.0	50.1					
	В	94.7	88.2	100.0	79.6					
	C	100.0	90.5	105.4	81.7					
	D	38.5	28.0	100.0	25.3					
	SYSTEM	100.8	87.5	100.0	78.9		720	650	568	
	** PROBLE	EMS/SOLUT	IONS/COMMENTS							
			THE UTILITY R	EPORTED THAT	THE UNIT WAS	REMOVED FR	OM SERV	ICE APR	PIL 28	FOR
/84	A	100.0			.0					
	В	100.0			.0					
	В	100.0			.0					
	C D	100.0			.0					
	SYSTEM	100.0			.0		744	0	0	
	** PROBLE	MS/SOLUT	IONS/COMMENTS		••		,	ŭ	J	
			THE UNIT REMA	INED OUT OF	SERVICE THROU	JGHOUT MAY DI	JE TO T	HE ANNU	JAL	
			MAINTENANCE O	UTAGE.						
/84	A B	.0 57.2		99.7	.0 51.0					
	Č	56.9		98.7	32.2					
	D	56.1		98.6	39.2					
	SYSTEM	56.8	77.5	99.0	40.8		720	379	294	
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			THE UTILITY R	EPORTED THAT	MODULE A WAS	BEING RELI	NED DUR	ING JUN	E.	
/84	A	62.5	53.5	100.0	53.5					
	B C	100.0	50.3	100.0	50.3					
	מ	100.0	34.4	100.0	34.4					
	SYSTEM	100.0 100.0	82.1 73.4	100.0 100.0	82.1 7 <b>3.</b> 4		744	744	546	
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			RELINING CONT	INUED AT MOD	ULE A DURING	JULY.				
/84		94.0	40.5	100.0	40.1					
	В	100.0	65.2	100.0	64.5					
	С	85.6	21.7		0112					

			PERFORMA	NCE DATA					
PERIOD MODULE	<b>AVAILABILITY</b>	OPERABILITY	RELIABILITY	UTILIZATION	% REMOVAL	PER	BOILER	FGD	CAP.
					SO2 PART.	HOURS	HOURS	HOURS	FACTOR
D	88.3	72.6	100.0	71.9					
SYSTEM	100.0	66.7	100.0	66.0		744	737	491	

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD RELATED PROBLEMS AROSE IN AUGUST.

9/84 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR SEPTEMBER 1984.

# SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

DESIGN AND PERFORMANCE DATA ; OR OF CHARLES DATA

COMPANY NAME	CINCINNATI GAS	# FIFCTRIC
COMPANY NAME	EAST BEND	W ELLO MAI
PLANT NAME		
UNIT NUMBER	2	
CITY	RABBIT HASH	
STATE	KENTUCKY	
REGULATORY CLASSIFICATION	C	
PARTICULATE EMISSION LIMITATION - NG/J		( .100 LB/MMBTU)
SO2 EMISSION LIMITATION - NG/J	516.	( 1.200 LB/MMBTU)
NOX EMISSION LIMITATION - NG/J	301.	( .700 LB/MMBTU)
NET PLANT GENERATING CAPACITY - MW	650	
GROSS UNIT GENERATING CAPACITY - MW	650	
NET UNIT GENERATING CAPACITY W/FGD - MW	600	
NET UNIT GENERATING CAPACITY WO/FGD - MW	619	
EQUIVALENT SCRUBBED CAPACITY - MW	650	
** UNIT DATA - BOILER AND STACK		
BOILER SUPPLIER	BABCOCK & WILC	nχ
BOILER TYPE	PULVERIZED COA	
BOILER SERVICE LOAD	BASE	
DESIGN BOILER FLUE GAS FLOW - CU.M/S	1763.96	(3738000 ACFM)
BOILER FLUE GAS TEMPERATURE - C	357.2	( 675 F)
	- · · · <del>-</del>	
STACK HEIGHT M	198.	( 650 FT)
STACK SHELL	CONCRETE	
STACK TOP DIAMETER - M	7.2	( 23.5 FT)
<b>_</b> .		
** FUEL DATA		
FUEL TYPE	COAL	
FUEL GRADE	BITUMINOUS	
AVERAGE HEAT CONTENT - J/G	2 <b>5</b> 586.	( 11000 BTU/LB)
RANGE HEAT CONTENT - BTU/LB		10800-13000
AVERAGE ASH CONTENT - %	11.90	
RANGE ASH CONTENT - %	9.0-14.0	
AVERAGE MOISTURE CONTENT %- %	10.00	
RANGE MOISTURE CONTENT - %	9.0-11.0	
AVERAGE SULFUR CONTENT - %	2.60	
AVERAGE SULFUR CONTENT - % RANGE SULFUR CONTENT - %	2.60	
RANGE SULFUR CONTENT - %	1.0-4.0	
RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - %	1.0-4.0 ******	
RANGE SULFUR CONTENT - %	1.0-4.0	
RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - %	1.0-4.0 ******	
RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - %	1.0-4.0 ******	
RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - % *** PARTICLE CONTROL	1.0-4.0 ******	
RANSE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - %  *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR	1.0-4.0 ******* ******	
RANSE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - %  *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER	1.0-4.0 ****** ******	
RANSE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - %  *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR	1.0-4.0 ******* ******	
RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - %  *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE	1.0-4.0 ****** ******	
RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - %  *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER	1.0-4.0 ******* ******* 0 NONE	
RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - %  *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER NUMBER	1.0-4.0 ******* ******* 0 NONE	
RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - %  *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER	1.0-4.0 ******* ******* 0 NONE	
RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - %  *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER NUMBER TYPE	1.0-4.0 ******* ******* 0 NONE	
RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - %  *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER NUMBER TYPE  ** ESP	1.0-4.0 ******* ******  0 NONE	
RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - %  *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER NUMBER TYPE  ** ESP NUMBER	1.0-4.0 ******* ******  0 NONE  0 NONE	
RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - %  *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER NUMBER TYPE  ** ESP NUMBER NUMBER NUMBER NUMBER OF SPARES	1.0-4.0 *******  0 NONE  0 NONE	
RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - %  *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER NUMBER TYPE  ** ESP NUMBER NUMBER NUMBER OF SPARES TYPE	1.0-4.0 *******  0 NONE  0 NONE  1 0 HOT SIDE	
RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - %  *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER NUMBER TYPE  ** ESP NUMBER NUMBER NUMBER NUMBER NUMBER NUMBER SUPPLIER	1.0-4.0 *******  0 NONE  0 NONE	DIVISION, JOY
RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - %  *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER NUMBER TYPE  ** ESP NUMBER NUMBER NUMBER OF SPARES TYPE	1.0-4.0 *******  0 NONE  0 NONE  1 0 HOT SIDE	DIVISION, JOY (3738000 ACFM)
RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - %  *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER NUMBER TYPE  ** ESP NUMBER NUMBER NUMBER NUMBER NUMBER NUMBER SUPPLIER	1.0-4.0 *******  0 NONE  0 NONE  1 0 HOT SIDE WESTERN PREC.	· · · · · · · · · · · · · · · · · · ·
RANGE SULFUR CONTENT - X AVERAGE CHLORIDE CONTENT - X RANGE CHLORIDE CONTENT - X  *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER NUMBER TYPE  ** ESP NUMBER NUMBER NUMBER NUMBER OF SPARES TYPE SUPPLIER INLET FLUE GAS CAPACITY - CU.M/S	1.0-4.0 *******  0 NONE  0 NONE  1 0 HOT SIDE WESTERN PREC. 1764.0	(3738000 ACFM)
RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - %  *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER NUMBER TYPE  ** ESP NUMBER NUMBER NUMBER NUMBER SUPPLIER INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE - C	1.0-4.0 *******  0 NONE  0 NONE  1 0 HOT SIDE WESTERN PREC. 1764.0 357.2	(3738000 ACFM) ( 675 F)
RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - % *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER NUMBER TYPE  ** ESP NUMBER NUMBER NUMBER NUMBER INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE - C PRESSURE DROP KPA PARTICLE REMOVAL EFFICENCY - %	1.0-4.0 *******  0 NONE  0 NONE  1 0 HOT SIDE WESTERN PREC. 1764.0 357.2 .1	(3738000 ACFM) ( 675 F)
RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - %  *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER NUMBER TYPE  ** ESP NUMBER NUMBER NUMBER NUMBER SUPPLIER INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE - C PRESSURE DROP KPA	1.0-4.0 *******  0 NONE  0 NONE  1 0 HOT SIDE WESTERN PREC. 1764.0 357.2 .1	(3738000 ACFM) ( 675 F)
RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - % *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER NUMBER TYPE  ** ESP NUMBER NUMBER NUMBER NUMBER INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE - C PRESSURE DROP KPA PARTICLE REMOVAL EFFICENCY - %	1.0-4.0 *******  0 NONE  0 NONE  1 0 HOT SIDE WESTERN PREC. 1764.0 357.2 .1	(3738000 ACFM) ( 675 F)
RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - % *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER NUMBER TYPE  ** ESP NUMBER NUMBER NUMBER NUMBER OF SPARES TYPE SUPPLIER INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE - C PRESSURE DROP KPA PARTICLE REMOVAL EFFICENCY - %  ** PARTICLE SCRUBBER	1.0-4.0 *******  0 NONE  0 NONE  1 0 HOT SIDE WESTERN PREC. 1764.0 357.2 .1 99.6	(3738000 ACFM) ( 675 F)
RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - % *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER NUMBER TYPE  ** ESP NUMBER NUMBER OF SPARES TYPE SUPPLIER INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE - C PRESSURE DROP KPA PARTICLE REMOVAL EFFICENCY - %  ** PARTICLE SCRUBBER NUMBER	1.0-4.0 *******  0 NONE  0 NONE  1 0 HOT SIDE WESTERN PREC. 1764.0 357.2 .1 99.6  0 NONE	(3738000 ACFM) ( 675 F)
RANGE SULFUR CONTENT - X AVERAGE CHLORIDE CONTENT - X RANGE CHLORIDE CONTENT - X  *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER NUMBER TYPE  ** ESP NUMBER NUMBER NUMBER OF SPARES TYPE SUPPLIER INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE - C PRESSURE DROP KPA PARTICLE SCRUBBER NUMBER GENERIC TYPE SPECIFIC TYPE	1.0-4.0 *******  0 NONE  0 NONE  1 0 HOT SIDE WESTERN PREC. 1764.0 357.2 .1 99.6  0 NONE	(3738000 ACFM) ( 675 F)
RANGE SULFUR CONTENT - X AVERAGE CHLORIDE CONTENT - X RANGE CHLORIDE CONTENT - X *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER NUMBER TYPE  ** ESP NUMBER NUMBER NUMBER OF SPARES TYPE SUPPLIER INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE - C PRESSURE DROP KPA PARTICLE REMOVAL EFFICENCY - X  ** PARTICLE SCRUBBER NUMBER GENERIC TYPE SPECIFIC TYPE TRADE NAME/COMMON NAME	1.0-4.0 *******  0 NONE  0 NONE  1 0 HOT SIDE WESTERN PREC. 1764.0 357.2 .1 99.6  0 NONE	(3738000 ACFM) ( 675 F)
RANGE SULFUR CONTENT - X AVERAGE CHLORIDE CONTENT - X RANGE CHLORIDE CONTENT - X  *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER NUMBER TYPE  ** ESP NUMBER NUMBER NUMBER INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE - C PRESSURE DROP KPA PARTICLE REMOVAL EFFICENCY - X  ** PARTICLE SCRUBBER NUMBER GENERIC TYPE SPECIFIC TYPE TRADE NAME/COMMON NAME SHELL GENERIC MATERIAL	1.0-4.0 ******  0 NONE  0 NONE  1 0 HOT SIDE WESTERN PREC. 1764.0 357.2 .1 99.6  0 NONE N/A N/A N/A	(3738000 ACFM) ( 675 F)
RANGE SULFUR CONTENT - X AVERAGE CHLORIDE CONTENT - X RANGE CHLORIDE CONTENT - X  *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER NUMBER TYPE  ** ESP NUMBER NUMBER NUMBER INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE - C PRESSURE DROP KPA PARTICLE REMOVAL EFFICENCY - X  ** PARTICLE SCRUBBER NUMBER GENERIC TYPE SPECIFIC TYPE TRADE NAME/COMMON NAME SHELL GENERIC MATERIAL SHELL SPECIFIC MATERIAL	1.0-4.0 *******  0 NONE  0 NONE  1 0 HOT SIDE WESTERN PREC. 1764.0 357.2 .1 99.6  0 NONE N/A N/A N/A N/A	(3738000 ACFM) ( 675 F)
RANGE SULFUR CONTENT - X AVERAGE CHLORIDE CONTENT - X RANGE CHLORIDE CONTENT - X  *** PARTICLE CONTROL  ** MECHANICAL COLLECTOR NUMBER TYPE  ** FABRIC FILTER NUMBER TYPE  ** ESP NUMBER NUMBER NUMBER INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE - C PRESSURE DROP KPA PARTICLE REMOVAL EFFICENCY - X  ** PARTICLE SCRUBBER NUMBER GENERIC TYPE SPECIFIC TYPE TRADE NAME/COMMON NAME SHELL GENERIC MATERIAL	1.0-4.0 ******  0 NONE  0 NONE  1 0 HOT SIDE WESTERN PREC. 1764.0 357.2 .1 99.6  0 NONE N/A N/A N/A	(3738000 ACFM) ( 675 F)

#### *** FGD SYSTEM

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** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                               THROWAWAY PRODUCT
                                               WET SCRUBBING
   SO2 REMOVAL MODE
   PROCESS TYPE
                                               LIME
   PROCESS ADDITIVES
                                               NONE
   SYSTEM SUPPLIER
                                               BABCOCK & WILCOX
   Δ-F FTRM
                                               SARGENT & LUNDY
   DEVELOPMENT LEVEL
                                               FULL SCALE
   NEW/RETROFIT
                                               NEW
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.00
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - X
                                                  87.00
   FNERGY CONSUMPTION - %
                                                   2.9
   CURRENT STATUS
   COMMERCIAL START-UP
                                                3/81
   INITIAL START-UP
                                                3/81
   CONTRACT AWARDED
                                                3/78
** DESIGN AND OPERATING PARAMETERS
   DESIGN COAL SULFER CONTENT - %
                                                  5.10
                                               25586.0
   DESIGN COAL HEAT CONTENT - J/G
                                                              ( 11000 BTU/LB)
    DESIGN COAL ASH CONTENT - %
                                                  11.90
   DESIGN MOISTURE CONTENT - %
                                                  10.00
    SPACE REQUIREMENTS - SQ M
                                               13461.2
                                                              ( 144900 SQ FT)
    OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                 144.0
** QUENCHER/PRESATURATOR
   NUMBER
   TYPF
                                               VENTURT
    SUPPLIER
                                               BABCOCK & WILCOX
    INLET GAS FLOW - CU. M/S
                                                 398.49 ( 844433 ACFM)
    INLET GAS TEMPERATURE - C
                                                 136.7
                                                              ( 278 F)
    PRESSURE DROP - KPA
                                                    . 2
                                                             ( 1.0 IN-H20)
    LIQUID RECIRCULATION RATE - LITERS/S
                                                 552.
                                                              ( 8760 GPM)
    L/G RATIO - L/CU. M
                                                   1.3
                                                              ( 10.0 GAL/1000 ACFM)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               AISI 1110
** ABSORBER
   NUMBER
                                                3
   NUMBER OF SPARES
                                                Λ
    GENERIC TYPE
                                               COUNTER CURRENT TRAY TOWER
    SPECIFIC TYPE
                                               SIEVE TRAY
    TRADE NAME/COMMON TYPE
                                               N/A
                                               BABCOCK & WILCOX
    SUPPLIER
                                               43.0 DIA X 95.0
    DIMENSIONS - FT
    SHELL GENERIC MATERIAL
                                               STATNIESS STEEL
    SHELL SPECIFIC MATERIAL
                                               AUSTENITIC
                                               TYPE 316
    SHELL MATERIAL TRADE NAME/COMMON TYPE
    LINER GENERIC MATERIAL
                                               NΔ
    LINER SPECIFIC MATERIAL
                                               NΔ
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                               NΔ
    GAS CONTACTING DEVICE TYPE
                                               PERFORATED TRAYS
    NUMBER OF CONTACTING ZONES
                                                1
    LIQUID RECIRCULATION RATE - LITER/S
                                                2205.
                                                              (35000 GPM)
                                                  6.7
    L/G RATIO - L/CU.M
                                                              ( 50.0 GAL/1000 ACF)
                                                              ( 2.5 IN-H2O)
    GAS-SIDE PRESSURE DROP KPA
                                                   .6
    SUPERFICAL GAS VELOCITY - M/SEC
                                                   2.4
                                                              ( 8.0 FT/S)
    INLET GAS FLOW - CU. M/S
                                                 329.66
                                                              ( 698585 ACFM)
                                                  50.6
                                                              ( 123 F)
   INLET GAS TEMPERATURE - C
   SO2 REMOVAL EFFICIENCY - X
                                                  87.0
** MIST ELIMINATOR
   PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                               PRIMARY COLLECTOR
   NUMBER PER SYSTEM
                                                6
   NUMBER OF SPARES PER SYSTEM
                                                n
   NUMBER PER MODULE
                                                2
   GENERIC TYPE
                                               IMPINGEMENT
   SPECIFIC TYPE
                                               BAFFLE
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TRADE NAME/COMMON TYPE
                                              CLOSED VANE
                                              BABCOCK & WILCOX
   MANUFACTURER
                                              HORIZONTAL
   CONFIGURATION
   NUMBER OF STAGES
   NUMBER OF PASSES PER STAGE
                                                  2.13
                                                           ( 7.0 FT)
   FREEBOARD DISTANCE - M
                                                            (72.0 IN)
   DISTANCE BETWEEN STAGES - CM
                                                182.88
                                                            ( 3.00 IN)
   DISTANCE BETWEEN VANES - CM
                                                 7.6
   VANE ANGLES - DEGREES
                                                90
   PRESSURE DROP - KPA
                                                             ( .5 IN-H20)
   SUPERFICAL GAS VELOCITY - M/S
                                                  2.4
                                                            ( 8.0 FT/S)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              ORGANIC
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              FIBER-REINFORCED POLYESTER
                                              BLENDED
   WASH WATER SOURCE
   WASH FREQUENCY
                                              INTERMITTENT
   WASH RATE - L/S
                                                 58.4
                                                           ( 926 GAL/MIN)
** REHEATER
   NUMBER
                                               1
   NUMBER OF SPARES
                                               0
   NUMBER PER MODULE
                                               0
   GENERIC TYPE
                                              INDIRECT HOT AIR
   SPECIFIC TYPE
                                              STEAM
   TRADE NAME/COMMON TYPE
                                              STEAM TUBE BUNDLE
   LOCATION
                                              PLENUM COMBINING GAS FLOW FROM INDIVIDUAL ABSORB
                                               13.9 ( 25 F)
51.7 ( 125 F)
   TEMPERATURE INCREASE - C
   INLET FLUE GAS TEMPERATURE - C
   NUMBER OF HEAT EXCHANGER BANKS
                                                 2
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              NΛ
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                             NA
** FANS
   NUMBER
                                               4
   NUMBER OF SPARES
                                               0
   DESTGN
                                              CENTRIFUGAL
   SUPPLIER
                                              WESTINGHOUSE
   FUNCTION
                                              UNIT
   APPLICATION
                                              INDUCED DRAFT
   SERVICE
                                              DPY
   FLUE GAS FLOW RATE - CU.M/S
                                              1175.12
                                                            (2490185 ACFM)
   FLUE GAS TEMPERATURE C
                                                            ( 278 F)
                                                136.7
   PRESSURE DROP - KPA
                                                  7.3
                                                            (23.8 IN-H20)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              CARBON STEEL
** FANS
   NUMBER
                                               2
   NUMBER OF SPARES
                                               0
   DESIGN
                                              CENTRIFUGAL
   SUPPLIER
                                              WESTINGHOUSE
   FUNCTION
                                              UNIT
   APPLICATION
                                              FORCED DRAFT
   SERVICE
                                              DRY
   FLUE GAS FLOW RATE - CU.M/S
                                              639.25
                                                            (1354635 ACFM)
   FLUE GAS TEMPERATURE - C
                                                37.8
                                                            ( 100 F)
   PRESSURE DROP KPA
                                                 5.3
                                                             (17.5 IN-H20)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                             CARBON STEEL
** FANS
   NUMBER
                                               3
   NUMBER OF SPARES
                                               Λ
   DESIGN
                                              CENTRIFUGAL
   SUPPLIER
                                              WESTINGHOUSE
   FUNCTION
                                              BOOSTER
   APPLICATION
                                              INDUCED DRAFT
   SERVICE
                                              DRY
   CONSTRUCTION MATERIAL GENERIC TYPE
                                             CARBON STEEL
** DAMPERS
   NUMBER
   FUNCTION
                                              SHUT-OFF
   GENERIC TYPE
                                              LOUVER
```

OPPOSED BLADE SPECIFIC TYPE MANUFACTURER BABCOCK & WILCOX MODUL ATTON OPEN SERVICE CONDITIONS 278 CARBON STEEL CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE NR LINER GENERIC MATERIAL TYPE NR LINER SPECIFIC MATERIAL TYPE NR

#### ** DAMPERS

FUNCTION CONTROL MODULATION OPEN

#### ** DUCTWORK

LOCATION AFTER SCRUBBER
CONFIGURATION CIRCULAR
DIMENSIONS 17 FT. DIAMETER
SHELL GENERIC MATERIAL TYPE CARBON STEEL
SHELL SPECIFIC MATERIAL TYPE NR
LINER GENERIC MATERIAL TYPE NR

LINER GENERIC MATERIAL TYPE NR
LINER SPECIFIC MATERIAL TYPE 40 MILS PLASITE 4005/2 INCHES KAOCRETE HS

#### ** REAGENT PREPARATION EQUIPMENT

FUNCTION SLAKER

DEVICE COMPARTMENTED

DEVICE TYPE PASTE

MANUFACTURER WALLACE & TIERNAN

NUMBER 8

NUMBER 0F SPARES 2

FULL LOAD DRY FEED CAPACITY - M.TONS/HR 3.6 ( 4 TPH)
PRODUCT QUALITY - % SOLIDS 15.8

#### ** TANKS

SERVICE NUMBER
----ABSORBER RECYCLE 3
REAGENT PREP PRODUCT 1
THICKENER OVERFLOW 1
THICKENER UNDERFLOW 1

# ** PUMPS

SERVICE NUMBER

FEED SLURRY

ABSORBER RECIRCULATION

QUENCHER RECIRCULATION

THICKENER UNDERFLOW

CLARIFIED RECYCLE

NUMBER

----
2

AUMBER

----
6

THICKENER UNDERFLOW

4

CLARIFIED RECYCLE

2

# ** SOLIDS CONCENTRATING/DEWATERING

OUTLET STREAM DISPOSITION

OVERFLOW STREAM DISPOSITION

VACUUM FILTER DEVICE NUMBER 4 NUMBER OF SPARES n CONFIGURATION HORIZONTAL-PARALLEL 12 FT. DIAMETER X 20 FT. DIMENSIONS FT 22 TONS/HR CAPACITY SHELL GENERIC MATERIAL TYPE CARBON STEEL AISI 1110 SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE OPGANTO POLYPROPYLENE LINER SPECIFIC MATERIAL TYPE BELT GENERIC MATERIAL TYPE RUBBER BELT SPECIFIC MATERIAL TYPE USBM 28 THICKENER UNDERFLOW FEED STREAM SOURCE 668 GPM, 30% SOLIDS 47.5% SOLIDS FEED STREAM CHARACTERISTICS OUTLET STREAM CHARACTERISTICS 200 GPM, 30% SOLIDS OVERFLOW STREAM CHARACTERISTICS

THICKENERS

MIXED WITH FLYASH & LIME

```
** SOLIDS CONCENTRATING/DEWATERING
                                                      THICKENER
     DEVICE
     NUMBER
                                                       2
                                                      Ω
     NUMBER OF SPARES
                                                      CYLINDRICAL
     CONFIGURATION
                                                     190.0 DIA X 25.0
     DIMENSIONS - FT
                                                     5000000 GALLONS
     CAPACITY
     SHELL GENERIC MATERIAL TYPE
                                                     CARBON STEEL
                                                  N/A
POLYESTER RESIN
     SHELL SPECIFIC MATERIAL TYPE
     LINER GENERIC MATERIAL TYPE
                                                  FLAKE GLASS
     LINER SPECIFIC MATERIAL TYPE
     BELT GENERIC MATERIAL TYPE
BELT SPECIFIC MATERIAL TYPE
     BELT GENERIC MATERIAL TYPE

BELT SPECIFIC MATERIAL TYPE

FEED STREAM SOURCE

FEED STREAM CHARACTERISTICS

OUTLET STREAM CHARACTERISTICS

OUTLET STREAM CHARACTERISTICS

OUTLET STREAM CHARACTERISTICS

OUTLET STREAM DISPOSITION

DUTHER STREAM DISPOSITION

PUMPED TO WASTE STABILIZATION SYSTEM
                                                     N/A
     OUTLET STREAM DISPOSITION
     OVERFLOW STREAM DISPOSITION
                                                     RECYCLED.
*** SLUDGE
     FULL LOAD SLUDGE QUANTITY - M.TONS/HR (DRY) 16.6 ( 18.3 TPH)
                                                          75.0
     MOISTURE CONTENT - % TOTAL FREE WATER
     % CASO3 - DRY
                                                          77.0
     % CASO4 - DRY
                                                          17.0
     % CAOH2 - DRY
                                                          3.0
     % CACO3 - DRY
                                                           1 0
     % ASH DRY
                                                           .0
     % SODIUM COMPOUNDS - DRY
                                                            . 0
     % OTHER COMPOUNDS - DRY
                                                           2.0
 ** TREATMENT
     METHOD
                                                      FTXATTON
     DEVICE
                                                      PUG MILL
     PROPRIETARY PROCESS
                                                      CONVERSION SYSTEMS [POZ-O-TEC]
     INLET FLOW RATE - LITER/S
                                                       42.1 ( 668 GPM)
     INLET QUALITY - %
                                                          30 0
 ** DISPOSAL
     NATURE
                                                      FINAL
     TYPE
                                                      LANDETIL
     LOCATION
                                                      ON-SITE
     SITE TRANSPORTATION METHOD
                                                      TRUCK
     SITE TREATMENT
                                                      UNLINED
     SITE DIMENSIONS
                                                     160 ACRES/120 FEET
     SITE CAPACITY - CU.M
                                                       23481600 ( 19200.0 ACRE-FT)
     SITE SERVICE LIFE - YRS
 ** WATER BALANCE
     WATER LOOP TYPE
     WATER LOOP TYPE

EVAPORATION WATER LOSS - LITER/S

SLUDGE HYDRATION WATER LOSS - LITER/S

SLUDGE INTERSTITIAL WATER LOSS - LITERS/S

6.9

( 348 GPM)

7 GPM)

109 GPM)
                                                    CLOSED
     POND SEEPAGE/RUNOFF WATER LOSS - LITERS/S 0
                                                     .0
NONE
     EFFLUENT WATER LOSS - LITERS/S
                                                                      ( 0 GPM)
     RECEIVING WATER STREAM
     MAKEUP WATER ADDITION - LITERS/S
                                                        29.2
                                                                     ( 464 GPM)
     SOURCE OF MAKEUP WATER
                                                    OHIO RIVER
 ** CHEMICALS AND CONSUMPTION
     FUNCTION
                                                      ABSORBENT
     NAME
                                                      THIOSORBIC LIME
     PRINCIPAL CONSTITUENT
                                                      90% CAO, 5% MGO, 5% INERT
     SOURCE/SUPPLIER
                                                      DRAVO LIME
     CONSUMPTION
                                                      250 TONS/DAY
     UTILIZATION - %
                                                          96.6
     POINT OF ADDITION
                                                       RECIRCULATION TANK
```

S A M R F S E R T	CRUBBER BSORBER IST ELIM EHEATER AN - % LAKER - FFLUENT ECIRCULA HICKENER	- % INATOR - % - % - % HOLD TANK - TION PUMP -	%		.0 .0 .0 .0 .0 25.0 .0 25.0					
S A M R F S E R T	CRUBBER ABSORBER AIST ELIM REHEATER FAN SLAKER EFFLUENT	HOLD TANK TION PUMP	ND ICES		.0 .0 .0 .0 .0 2.0 .0 3.0					
			Y OPERABILITY			% REMOVA	L PER	BOILER	FGD	CAP.
						SO2 PAR				FACTOR
3/81	A R	98.3 97.6	55.3 48.4 ∍ .0 51.8	100.0	14.1 12.4					
	Č	74.4	.J .O	100.0	.0					
	SYSTEM	100.0	<b>5</b> 1.8	100.0	13.2	47.70	744	190	99	12.6
			ONS/COMMENTS							
			THE FGD SYSTEM					IN MARCI	H 1981.	МО
4/81	A	96.3	69.2	100.0	59.0					
	В	89.7	50.6 47.9	100.0	43.2					
	C	86.3	47.9	100.0	40.8					
	SYSTEM	100.0	83.8	100.0	71.5	78.70	720	614	515	60.4
5/81	A	84.5	76.6	100.0	60.3					
	В	71.5	76.6 35.9	100.0	28.2					
	C	41.2	10.3	100.0	8.1			=-/		
	SYSTEM	98.6	61.5	100.0	48.3	96.10	744	586	360	41.4
6/81	A	100.0	82.4	100.0	70.5					
	В	67.8	44.8	100.0	38.3					
	C	94.9	72.0	100.0	61.6	96. ( 9	700	(1)	(36	(0.1
	SYSTEM	100.0	99.6	100.0	85.2	84.60	720	616	614	62.6
	** PROB	LEMS/SOLUTION	DNS/COMMENTS							
			THE UTILITY RE		THE FGD SYS	TEM HAS OF	ERATED S	INCE MI	D-MARCH	HTIW H
7/81	Δ	89.3	56.4	100.0	56.3					
	В	91.7	72.0	100.0	71.9					
	С	97.4	57.2	100.0	57.1					
	SYSTEM	100.0	92.7	100.0	92.6	92.40	744	743	689	79.6
8/81	Δ	45.9	15.8	100.0	15.3					
2, 31	B	96.0	92.5	100.0	89.7					
	Č	97 <b>.5</b>	81.8	100.0	79.3					
	SYSTEM	100.0	95. <b>0</b>	100.0	92.1	82.30	744	721	685	76.2

** PROBLEMS/SOLUTIONS/COMMENTS

99.**0** 

100.0

100.0

100.0

7/82 SYSTEM

8/82 SYSTEM

PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% REI SO2	MOVAL PART.	PER HOURS	HOURS	HOURS	FACTOR
9/81	A	85.7	67.5 84.6 10.4 81.3	100.0	62.9						
	В	96 - 6	84.6	100.0	78.8						
	С	33.5	10.4	100.0	9.7						
	SYSTEM	100.0	81.3	100.0	75.7	77.40		720	671	545	65.3
	** PROB	BLEMS/SOLUTIO	NS/COMMENTS								
		7	THE ONLY PROB THE TWO THICK POND FOR A SH	ENERS. THE	PROBLEM NECES	SSITAT	D USE	OF THE	E EMERG	ENCY AS	SH .
		A L L	THE UTILITY REALISHED THE IS BEING LIME AS THE REALISHED CALLED THE SYSTEM CALLED TH	E MONTH PERIO USED. THE D EAGENT AND,	OD BEGINNING FGD SYSTEM W AS SUCH, THE	ON NI S DES: TESTI	VEMBER IGNED	. CURF	RENTLY, RATE WI	THIOSO TH STRA	RBIC LIGHT
10/81	Δ	92.4	31.4	100.0	29.3						
	В	97.6	89.3	100.0	83.3						
	ř	91.7	75.0	100.0	85 1						
	SYSTEM	100.0	89.3 75.0 97.8	100.0	91.3	81.60		744	695	679	68.2
	A										
	_	96.4	61.2 75.8	100.0	28.0						
	ř	96.4	12.6	100.0	4.6						
	SYSTEM	100.0	12.6 74.5	100.0	27.6	86.70		720	266	198	30.0
12/81	A	93.4		100.0 100.0 100.0							
	B	93.4	56.4	100.0	52 2						
	ř	81.0	63.1	100.0	58 4						
	SYSTEM	100.0	63.1 86.6	100.0	80.1	85.7 <b>0</b>		744	689	596	68.0
	** PROS	SLEMS/SOLUTIO	NS/COMMENTS								
		F	OURING THE FO FOR AN INSPEC CORROSION OR	TION. THE U	TILITY REPOR	TED TH	AT THE	RE WERE	E NO SI	SNS OF	ANY
1/82	A	64.1	57.6	100.0	50 5						
	В	97.0	94.5	100.0	82 B						
	Č	48.7	94.5 34.4	100.0	30 1						
	SYSTEM	100.0	93.2	100.0	81.8	80.60		744	653	608	75.9
	** PROE	BLEMS/SOLUTIO	NS/COMMENTS								
		C	OURING JANUAR	Y PROBLEMS W	ERE ENCOUNTE	RED WI	TH ICE	BUILD	ד אס פע	HE FANS	5.
2/82	SYSTEM							672			
3/82	SYSTEM							744			
4/82	SYSTEM							720			
5/82	SYSTEM							744			
6/82	SYSTEM							720			
								120			

100.0 100.0

100.0

INFORMATION WAS UNAVAILABLE FOR THE PERIOD OF MARCH 1982 TO JUNE 1982.

744 733 730 68.7

744 744 744 77.9

98.1

744

CINCINNATI GAS & ELECTRIC: EAST BEND 2 (CONT.)

12/83 SYSTEM

PERIOD			OPERABILITY			% REMOV		BOILER	FGD	CAP.
		700.0		100.0	00.0		700			
9/82	SYSTEM		99.7	100.0	98.9		720	714	712	61.5
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS							
			THE UTILITY REDURING THE PE	_				WERE E	NCOUNTI	ERED
10/82	SYSTEM	100.0	100.0	100.0	2.5		744	19	19	1.6
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS							
		7	THE UNIT WAS	REMOVED FROM	SERVICE DURI	ING OCTOE	BER FOR A	MAINTEN	ANCE O	JTAGE.
11/82	SYSTEM	100.0		100.0			720	0		
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
		-	DUTAGE TIME D THE MAINTENAN CIENT FOR OPE	CE OUTAGE IN	OCTOBER. BO	DILER OUT	LET TEMPE			
12/82	SYSTEM	100.0	99.4	100.0	95.6		744	715	711	52.2
1/83	SYSTEM	100.0	99.7	100.0	98.4		744	734	732	67.1
2/83	SYSTEM	100.0	100.0	100.0	100.0		672	672	672	74.5
3/83	SYSTEM	100.0	98.9	100.0	89.9		744	677	669	69.2
4/83	SYSTEM	100.0	98.6	100.0	75.1		720	547	541	71.2
5/83	SYSTEM	100.0	99.2	100.0	99.2		744	741	738	91.8
6/83	SYSTEM	100.0	99.4	100.0	90.4		720	655	651	81.7
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
			THE UTILITY R DURING THE PE					WERE E	исоинті	ERED
7/83	SYSTEM	100.0	99.5	100.0	92.9		744	694	691	80.1
8/83	SYSTEM	100.0	99.7	100.0	99.5		744	742	740	85.5
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS							
			THE UTILITY R DURING JULY A		NO MAJOR FG	O-RELATED	PROBLEMS	WERE E	NCOUNT	ERED
9/83	SYSTEM						720			
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
		:	INFORMATION W	AS UNAVAILAB	LE FOR THE MO	ONTH OF S	SEPTEMBER.			
10/83	SYSTEM						744			
11/83	SYSTEM						720			

UTILITY FGD SURVEY: OCTOBER 1983 - SEPTEMBER 1984

CINCINNATI GAS & ELECTRIC: EAST BEND 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

#### ** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE REPORTED DURING THE FOURTH QUARTER OF 1983. AVAILABILITY WAS REPORTED AS 100%.

1/84	SYSTEM	744
2/84	SYSTEM	696
3/84	SYSTEM	744
4/84	SYSTEM	720
5/84	SYSTEM	744
6/84	SYSTEM	720
7/84	SYSTEM	744
8/84	SYSTEM	744
9/84	SYSTEM	720

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE FGD SYSTEM WAS 100% AVAILABLE DURING THE FIRST THREE QUARTERS OF 1984.

# SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COLORADO UTE ELECTRIC COMPANY NAME PLANT NAME CRAIG UNIT NUMBER CITY CRAIG STATE COLORADO REGULATORY CLASSIFICATION 43. ( .100 LB/MMBTU) 172. ( .400 LB/MMBTU) 301. ( .700 LB/MMBTU) PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J 301. 900 455 NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW 400 NET UNIT GENERATING CAPACITY W/FGD - MW NET UNIT GENERATING CAPACITY WO/FGD - MW 406 EQUIVALENT SCRUBBED CAPACITY - MW 455 ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER BABCOCK & WILCOX BOILER TYPE PULVERIZED COAL BOILER SERVICE LOAD BASE 722.29 DESIGN BOILER FLUE GAS FLOW - CU.M/S (1530600 ACFM) BOILER FLUE GAS TEMPERATURE - C 121.1 ( 250 F) 183. ( 600 FT) STACK HEIGHT - M CONCRETE STACK SHELL 10.9 ( 35.8 FT) STACK TOP DIAMETER - M ** FUEL DATA FUEL TYPE COAL FUEL GRADE SUBBITUMINOUS AVERAGE HEAT CONTENT - J/G 23260. ( 10000 BTU/LB) RANGE HEAT CONTENT - BTU/LB 9100-10300 AVERAGE ASH CONTENT - % 8.00 RANGE ASH CONTENT - % ***** AVERAGE MOISTURE CONTENT - % 16.00 RANGE MOISTURE CONTENT %
AVERAGE SULFUR CONTENT - % ***** RANGE SULFUR CONTENT - % 0.4-0.5 AVERAGE CHLORIDE CONTENT - % ****** RANGE CHLORIDE CONTENT - % 0.00-0.02 *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER Ω TYPE NONE ** ESP NUMBER 1 NUMBER OF SPARES n HOT SIDE SUPPLIER BELCO SUPPLIER
INLET FLUE GAS CAPACITY - CU.M/S (2950000 ACFM) ( 750 F) 1392.1 INLET FLUE GAS TEMPERATURE - C 398.**9** PRESSURE DROP - KPA ( 3. IN-H2O) .7 99.9 PARTICLE REMOVAL EFFICENCY - % ** PARTICLE SCRUBBER NUMBER NONE GENERIC TYPE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATEPIAL N/A SHELL SPECIFIC MATERIAL N/A N/A LINER GENERIC MATERIAL LINER SPECIFIC MATERIAL N/A GAS CONTACTING DEVICE TYPE N/A

*** FGD SYSTEM

SPECIFIC TYPE

```
** GENERAL DATA
      SALEABLE PRODUCT/THROWAWAY PRODUCT
                                                THROWAWAY PRODUCT
                                                 WET SCRUBBING
      SO2 REMOVAL MODE
                                                 LIMESTONE
      PROCESS TYPE
                                                 NONE
      PROCESS ADDITIVES
      SYSTEM SUPPLIER
                                                 PEABODY PROCESS SYSTEMS
                                                 STEARNS-ROGER
      A-E FIRM
      DEVELOPMENT LEVEL
                                                 FULL SCALE
      NEW/RETROFIT
                                                 NFW
      UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.80
      UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                   85.00
      ENERGY CONSUMPTION - %
                                                    1.3
      CURRENT STATUS
                                                 7
      COMMERCIAL START-UP
                                                 12/80
      INITIAL START-UP
                                                 10/80
      CONTRACT AWARDED
                                                  5/77
  ** DESIGN AND OPERATING PARAMETERS
      DESIGN COAL SULFER CONTENT - %
                                                      . 96
                                               22329.6
      DESIGN COAL HEAT CONTENT - J/G
                                                              ( 9600 BTU/LB)
      DESIGN COAL ASH CONTENT - %
                                                   11.60
      DESIGN MOISTURE CONTENT - X
                                                    15.30
      DESIGN CHLORIDE CONTENT - %
                                                     .10
      SPACE REQUIREMENTS - SQ M
                                                12140.2
                                                               ( 130680 SQ FT)
      OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                   264.0
.. ** QUENCHER/PRESATURATOR
      NUMBER
      TYPE
                                                 QUENCH DUCT
      SUPPLIER
                                                 PEABODY PROCESS SYSTEMS
      INLET GAS FLOW - CU. M/S
                                                 217.07 ( 460000 ACFM)
      INLET GAS TEMPERATURE - C
                                                   121.1
                                                              ( 250 F)
      PRESSURE DROP - KPA
                                                     ۰.2
                                                               ( 1.0 IN-H20)
      LIQUID RECIRCULATION RATE - LITERS/S
                                                               ( 500 GPM)
( 1.1 GAL/1000 ACFM)
                                                    31.
      L/G RATIO L/CU. M
                                                     .1
      CONSTRUCTION MATERIAL GENERIC TYPE
                                                HIGH ALLOY
      CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                NICKEL BASE/CHROMIUM-IRON-MOLYBDENUM
  ** ABSORBER
      NUMBER
                                                  4
      NUMBER OF SPARES
                                                  1
      GENERIC TYPE
                                                 SPRAY TOWER
      SPECIFIC TYPE
                                                 OPEN COUNTERCURRENT SPRAY
      TRADE NAME/COMMON TYPE
                                                 N/A
      SUPPLITER
                                                 PEABODY PROCESS SYSTEMS
      DIMENSIONS - FT
                                                 32.0 DIA X 52.5
      SHELL GENERIC MATERIAL
                                                 CARBON STEEL
      SHELL SPECIFIC MATERIAL
                                                 AISI 1110
      SHELL MATERIAL TRADE NAME/COMMON TYPE
                                                 N/A
      LINER GENERIC MATERIAL
                                                 ORGANIC (SPRAY ZONE); GLASS FLAKE-FILLED POLYEST
      LINER SPECIFIC MATERIAL
                                                 NATURAL RUBBER
      LINER MATERIAL TRADE NAME/COMMON TYPE
                                                 BLACK NATURAL RUBBER
      GAS CONTACTING DEVICE TYPE
                                                 NONE
      NUMBER OF CONTACTING ZONES
                                                  4
      LIQUID RECIRCULATION RATE - LITER/S
                                                  1512.
                                                              (24000 GPM)
      L/G RATIO - L/CU.M
                                                   7.0
                                                               ( 52.2 GAL/1000 ACF)
      GAS-SIDE PRESSURE DROP - KPA
                                                               ( 1.5 IN-H20)
                                                     .4
      SUPERFICAL GAS VELOCITY - M/SEC
                                                    3.0
                                                               ( 10.0 FT/S)
      INLET GAS FLOW - CU. M/S
                                                  217.07
                                                               ( 460000 ACFM)
      INLET GAS TEMPERATURE - C
                                                  121.1
                                                               ( 250 F)
      SO2 REMOVAL EFFICIENCY - %
                                                    85.0
      PARTICLE REMOVAL EFFICENCY - %
                                                    50.0
  ** MIST ELIMINATOR
      PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                                 PRIMARY COLLECTOR
      NUMBER PER SYSTEM
                                                  4
      NUMBER OF SPARES PER SYSTEM
                                                  1
      NUMBER PER MODULE
                                                  1
      GENERIC TYPE
                                                 IMPINGEMENT
```

BAFFLE

```
TRADE NAME/COMMON TYPE
                                               CLOSED VANE
   CONFIGURATION
                                               HORIZONTAL
   NUMBER OF STAGES
                                                   1
   NUMBER OF PASSES PER STAGE
                                                   4
   FREEBOARD DISTANCE - M
                                                   1.52
                                                              ( 5.0 FT)
   DISTANCE BETWEEN VANES - CM
                                                   3.0
                                                              ( 1.20 IN)
   VANE ANGLES - DEGREES
                                                 45
   PRESSURE DROP - KPA
                                                              ( 1.0 IN-H20)
   SUPERFICAL GAS VELOCITY - M/S
                                                   3.0
                                                              ( 10.0 FT/S)
                                               ORGANIC
   CONSTRUCTION MATERIAL GENERIC TYPE
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               POLYPHENYLENE
   WASH WATER SOURCE
                                               RAW WATER
   WASH FREQUENCY
                                               CONTINUOUS
   WASH RATE - L/S
                                                   6.3
                                                              ( 100 GAL/MIN)
** REHEATER
   NUMBER
                                                4
   NUMBER OF SPARES
                                                1
   NUMBER PER MODULE
                                                1
   GENERIC TYPE
                                               BYPASS
   SPECIFIC TYPE
                                               COLD SIDE
   TRADE~NAME/COMMON TYPE
                                               N/A
                                               OUTLET DUCT BETWEEN ME & OUTLET DAMPER
   LOCATION
   PERCENT GAS BYPASSED - AVG
                                                 23.0
                                                  27.8
   TEMPERATURE INCREASE C
                                                                 50 F)
   INLET FLUE GAS FLOW RATE - CU. M/S
                                                 194.89
                                                             ( 413000 ACFM)
    INLET FLUE GAS TEMPERATURE - C
                                                 43.3
                                                              ( 110 F)
    OUTLET FLUE GAS FLOW RATE - CU. M/S
                                                 302.02
                                                              ( 640000 ACFM)
   OUTLET FLUE GAS TEMPERATURE - C
                                                  73.9
                                                              ( 165 F)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                               STAINLESS STEEL
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               AUSTENITIC
** FANS
   NUMBER
                                                4
   NUMBER OF SPARES
                                                Λ
   DESIGN
                                               AXIAL
   SUPPLIER
                                               BUFFALO FORGE
   FUNCTION
                                               INDIRECT REHEAT
   APPLICATION
                                               N/A
   SERVICE
                                               DRY
                                                             ( 97545 ACFM)
   FLUE GAS FLOW RATE - CU.M/S
                                                 46.03
                                               CARBON STEEL
   CONSTRUCTION MATERIAL GENERIC TYPE
** FANS
   NUMBER
                                                4
   NUMBER OF SPARES
                                                1
   DESIGN
                                               AXIAL
   SUPPLIER
                                               BUFFALO FORGE
   FUNCTION
                                               BOOSTER
                                               FORCED DRAFT
   APPLICATION
                                               DRY
   SERVICE
                                                 372.80
                                                              ( 790000 ACFM)
   FLUE GAS FLOW RATE - CU.M/S
   FLUE GAS TEMPERATURE - C
                                                              ( 250 F)
                                                 121.1
   PRESSURE DROP - KPA
                                                              (11.0 IN-H20)
                                                   3 4
   CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL
** DAMPERS
                                                4
   NUMBER
   GENERIC TYPE
                                               PARALLEL BLADE MULTILOUVER
   SPECIFIC TYPE
   MANUFACTURER
                                               FORNEY ENGINEERING
   MODULATION
                                               OPEN
                                                              ( 6500 ACFM)
   SEAL AIR FLOW - CU. M/S
   CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL/STAINLESS STEEL
                                               ASTM A-285
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               NONE
   LINER GENERIC MATERIAL TYPE
                                               N/A
   LINER SPECIFIC MATERIAL TYPE
** DAMPERS
   NUMBER
   GENERIC TYPE
                                               LOUVER
```

PARALLEL BLADE MULTILOUVER SPECIFIC TYPE FORNEY ENGINEERING MANUFACTURER OPEN MODULATION ( 6500 ACFM) 3.07 SEAL AIR FLOW - CU. M/S CARBON STEEL/STAINLESS STEEL CONSTRUCTION MATERIAL GENERIC TYPE ASTM A-285 CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE NONE N/A LINER SPECIFIC MATERIAL TYPE ** DAMPERS NUMBER GENERIC TYPE LOUVER PARALLEL BLADE MULTILOUVER SPECIFIC TYPE FORNEY ENGINEERING MANUFACTURER MODULATION 3.07 ( 6500 ACFM) SEAL AIR FLOW - CU. M/S CARBON STEEL/STAINLESS STEEL CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE ASTM A-285 LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DAMPERS NUMBER GENERIC TYPE GUILLOTINE SPECIFIC TYPE NR MANUFACTURER FORNEY ENGINEERING MODULATION SEAL AIR FLOW - CU. M/S .00 { 0 ACFM) CARBON STEEL/HIGH ALLOY CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE AISI 1110; NR LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DAMPERS NUMBER 2 GENERIC TYPE LOUVER SPECIFIC TYPE PARALLEL BLADE MULTILOUVER MANUFACTURER FORNEY ENGINEERING MODULATION SEAL AIR FLOW CU. M/S .00 ( 0 ACFM) CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL/STAINLESS STEEL CONSTRUCTION MATERIAL SPECIFIC TYPE ASTM A-285 LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DAMPERS NUMBER 1 GENERIC TYPE LOUVER SPECIFIC TYPE PARALLEL BLADE MULTILOUVER MANUFACTURER FORNEY ENGINEERING MODULATION OPEN SEAL AIR FLOW - CU. M/S .00 ( 0 ACFM) CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL/STAINLESS STEEL CONSTRUCTION MATERIAL SPECIFIC TYPE ASTM A-285 LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DAMPERS NUMBER 2 GENERIC TYPE LOUVER SPECIFIC TYPE PARALLEL BLADE MULTILOUVER MANUFACTURER FORNEY ENGINEERING MODULATION CLOSED SEAL AIR FLOW - CU. M/S .00 1 0 ACEM1 CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL/STAINLESS STEEL CONSTRUCTION MATERIAL SPECIFIC TYPE ASTM A-285 LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A

** DUCTWORK  LOCATION  SHELL GENERIC MATERIAL TYPE  SHELL SPECIFIC MATERIAL TYPE  LINER GENERIC MATERIAL TYPE  LINER SPECIFIC MATERIAL TYPE	INLET TO QUENCH CARBON STEEL AISI 1110 NONE N/A
** DUCTWORK LOCATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	OUTLET TO DAMPER CARBON STEEL AISI 1110 ORGANIC GLASS FLAKE-FILLED POLYESTER
** DUCTWORK LOCATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	DAMPER TO STACK CARBON STEEL AISI 1110 NONE N/A
** DUCTWORK  LOCATION  SHELL GENERIC MATERIAL TYPE  SHELL SPECIFIC MATERIAL TYPE  LINER GENERIC MATERIAL TYPE  LINER SPECIFIC MATERIAL TYPE	BYPASS CARBON STEEL AISI 1110 NONE N/A
** REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE DEVICE TYPE MANUFACTURER NUMBER NUMBER NUMBER OF SPARES FULL LOAD DRY FEED CAPACITY - M.TONS/HR PRODUCT QUALITY - % SOLIDS	WET BALL MILL COMPARTMENTED NR KENNEDY VAN SAUN 1 0 9.1 ( 10 TPH) 35.0
** TANKS SERVICE ABSORBER RECYCLE REAGENT PREP PRODUCT THICKENER OVERFLOW CLASSIFIER OVERFLOW FLOCCULANT WASTE SLURRY BLEED	NUMBER 4 1 1 4 1 1 4
** PUMPS  SERVICE  RAW WATER  RECLAIM SUMP POND  COOLING TOWER BLOWDOWN BOOSTER  ABSORBER RECIRCULATION  WASH SLURRY  SUPERNATANT  THICKENER UNDERFLOW POLYELECTROLYTE  WASTE SLURRY  MILL RECIRCULATION  LIMESTONE SLURRY FEED	NUMBER  2 7 1 2 8 8 8 2 2 1 2 2
** SOLIDS CONCENTRATING/DEWATERING DEVICE NUMBER NUMBER OF SPARES DIMENSIONS - FT CAPACITY	CENTRIFUGE  1 1 3.0 DIA X 6.0 126 GPM

HIGH ALLOY NICKEL BASE/CHROMIUM-IRON-MOLYBDENUM SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE NONE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE N/A N/A BELT GENERIC MATERIAL TYPE BELT SPECIFIC MATERIAL TYPE N/A THICKENER UNDERFLOW FEED STREAM SOURCE FEED STREAM CHARACTERISTICS 35% SOLIDS
OUTLET STREAM CHARACTERISTICS 60% SOLIDS
OVERFLOW STREAM CHARACTERISTICS 60 GPM
OUTLET STREAM DISPOSITION LANDFILL TO WASTE SUMP & THEN TO THICKENER OVERFLOW STREAM DISPOSITION ** SOLIDS CONCENTRATING/DEWATERING THICKENER DEVICE 1 NUMBER NUMBER OF SPARES CONFIGURATION CENTER DRAW 75.0 DIA X 15.0 DIMENSIONS - FT CARBON STEEL SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE AISI 1110 ORGANIC LINER GENERIC MATERIAL TYPE GLASS FLAKE-FILLED POLYESTER [WALLS]; MAT-REINFO LINER SPECIFIC MATERIAL TYPE OUTLET STREAM CHARACTERISTICS 5% SOLIDS

OVERFLOW STREAM CHARACTERISTICS 100 GPM, <1% SUSPENDED SOLIDS

OUTLET STREAM DISPOSITION TO CENTRIFUGES

OVERFLOW STREAM DISPOSITION RECYCLED TO SOCIED FEED STREAM SOURCE ABSORBER BLEED *** SALEABLE BYPRODUCTS *** SLUDGE FULL LOAD SLUDGE QUANTITY - M.TONS/HR (DRY) 10.5 ( 11.6 TPH) MOISTURE CONTENT - % TOTAL FREE WATER 40.0 % CASO3 - DRY 22.6 % CASO4 - DRY 70.2 % CAOH2 - DRY . 0 % CACO3 - DRY 2.9 % ASH DRY . 3 % OTHER COMPOUNDS - DRY 3.9 ** TREATMENT METHOD NONE ** DISPOSAL NATURE FINAL TYPE LANDFILL LOCATION ON-SITE SITE TRANSPORTATION METHOD TRUCK ** PROCESS CONTROL AND INSTRUMENTATION CHEMICAL PARAMETERS PH, SO2 CONCENTRATION PHYSICAL VARIABLES DENSITY, GAS FLOH, LIQUID FLOW CONTROL LEVELS PH 5.4, SOLIDS 12-15% MONITOR TYPE UNILOK-PH, OHMART-DENSITY, BROOKS-FLOW, DYNASCIE MONITOR LOCATION AT MODULE RECYCLE TANK PROCESS CONTROL MANNER AUTOMATIC PROCESS CHEMISTRY MODE FFEDBACK ** WATER BALANCE WATER LOOP TYPE CLOSED EVAPORATION WATER LOSS LITER/S 17.8 ( 282 GPM) SLUDGE HYDRATION WATER LOSS LITER/S SLUDGE HYDRATION WATER LOSS LITER/S .6 ( 9 GPM)
SLUDGE INTERSTITIAL WATER LOSS - LITERS/S 2.1 ( 33 GPM) 9 GPM)

.0

( 0 GPM)

POND SEEPAGE/RUNOFF WATER LOSS - LITERS/S 0

EFFLUENT WATER LOSS - LITERS/S

RECEIVING WATER STREAM

MAKEUP WATER ADDITION - LITERS/S

SOURCE OF MAKEUP WATER

N/A

20.2 ( 321 GPM)

COOLING TOWER BLOWDOWN

** CHEMICALS AND CONSUMPTION

FUNCTION ABSORBENT
NAME LIMESTONE
PRINCIPAL CONSTITUENT CACO3
CONSUMPTION 7000 LB/HR
UTILIZATION - % 75.0
POINT OF ADDITION BALL MILL

** FGD SPARE CAPACITY INDICES

ABSORBER - % 33.3
MIST ELIMINATOR - % 33.3
REHEATER - % 33.3
BALL MILL - % .0
EFFLUENT HOLD TANK - % 33.3
THICKENER - % .0
CENTRIFUGE - % 50.0

** FGD SPARE COMPONENT INDICES

ABSORBER 1.0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

10/80 SYSTEM 744

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM BEGAN INITIAL OPERATIONS ON OCTOBER 9, 1980 WHEN MODULE D CAME ON LINE. HOWEVER MODULE'S A THROUGH C ARE STILL UNDER CONSTRUCTION.

11/80 D 48.6 44.7 46.2 38.5 SYSTEM 720 619 47.3

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER OPERATED AT ABOUT 50 TO 60% LOAD CAPACITY DURING NOVEMBER. ONLY ONE MODULE IS REQUIRED FOR COMPLIANCE WHEN OPERATING UNDER THE REDUCED LOAD CONDITION.

12/80	A	. 0	.0		.0
	В	53.8	44.3	70.4	42.6
	С	73.9	70.4	84.0	67.7
	D	60.5	56.0	80.2	53.9
	SYSTEM	62.7	56.8	78.7	54.7

STEM 62.7 56.8 78.7 54.7 744 716 407 63.0

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM EQUIPMENT CHECKOUT CONTINUED THROUGH DECEMBER. MODULE A NEEDED MECHANICAL PARTS FOR REPAIR. AS OF DECEMBER 23, THE PROBLEMS CAUSING LOAD RESTRICTION WERE CORRECTED AND THE UNIT INCREASED TO FULL LOAD.

1/81	A	.0	.0	.0	. 0	
	В	59.7	70.2	71.0	55.4	
	С	48.9	59.8	60.5	47.2	
	D	11.3	12.6	12.7	9.9	
	SYSTEM	39.9	47.5	48.1	37.5	744

#### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING JANUARY THE FGD SYSTEM EQUIPMENT CHECKOUT CONTINUED. MODULE A REMAINED OUT OF SERVICE BECAUSE THE MECHANICAL PARTS NEEDED FOR REPAIR WORK WERE NOT AVAILABLE.

587

279 62.0

ERIOD	MODULE		OPERABILITY		UTILIZATION	% REM	10VAL	PER	BOILER HOURS	FGD HOURS	CAP. FACTOR
2/81	В	.0 12.2	.0 12.4 12.4	.0 12.9 12.9	.0 10.7 10.7						
	C D	13.6		.0	.0						
	SYSTEM	.0 8.6	.0 8.3	8.6	7.1			672	<b>5</b> 8 <b>0</b>	36	64.2
		BLEMS/SOLUTIO									
	2. TRO	T	HE CHECKOUT (	ANICAL PARTS	YSTEM EQUIPME FOR REPAIR.						
			E OPERATING		ED PROBLEMS W		IE TNI I	ET AND	OUTLET	DAMDED	
			URING FEBRUA		ED PROBLEMS M	1110 IU	IE TIVLI	ET AND	001111	DAILPER	.3
3/81	A	.0	.0	.0	. 0						
	В	.0	.0	.0	.0						
	C	. 0	.0	.0	.0						
	D	35.5	35.5	35.7	35.5			744	766	0.0	00 (
	SYSTEM	11.8	11.8	11.9	11.8			/44	744	88	88.6
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			URING MARCH I AMPERS.	MODULES A, B	, AND C EXPER	IENCED	OPERA	ATING F	PROBLEMS	HTIW 6	THE
			DDITIONAL OU S.	TAGE TIME WAS	S DUE TO THE	READJU	ISTMEN	T OF TH	HE FAN E	BLADE F	TCH-
4/81		.0	.0	.0	.0						
	В	36.1	59.9	60.9	35.6						
	C D	2.8 <b>25.</b> 0	4.2 40.5	4.3	2.5						
	SYSTEM			41.2 26.6	23.9 20.7			720	427	149	52.9
	** PROB	BLEMS/SOLUTIO	NS/COMMENTS								
		ם	URING THE FI AMPERS AND CO ODULES WERE I	ONTROLS MALF	APRIL THE SYS UNCTIONING.	TEM EX	(PERIEI E A NEI	NCED PR	ROBLEMS ARTS AND	WITH TO THE C	HE OTHER
		_	N APRIL 18 TI UTAGE.	HE UNIT WAS	SHUT DOWN FOR	A SCH	IEDULEI	D FIVE	WEEK MA	AINTENA	NCE
5/81	SYSTEM	.0	.0	.0	.0			744	101	o	
6/81	SYSTEM	.0	.0	.0	.0			720	699	0	97.1
	** PROE	BLEMS/SOLUTIO	NS/COMMENTS								
		D E	URING MAY ANI LIMINATOR PAI	JUNE THE S	YSTEM WAS OUT ING OF THE MI	OF SE	RVICE MINAT	DUE TO	D DAMAGI	ED MIST	7
		Т	HICKENER REP	AIRS WERE PE	RFORMED DURIN	IG JUNE					
7/81	SYSTEM	.0	.0	.0	. 0			744	724	0	58.9
	** PROE	BLEMS/SOLUTIO	NS/COMMENTS								
			HE FGD SYSTE IST ELIMINAT		FF LINE THROU	IGH JUI	Y AS	A RESU	LT OF TI	HE BRO	KEN

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

#### ** PROBLEMS/SQLUTTONS/COMMENTS

AS OF THE END OF AUGUST, MODULES A AND C WERE READY FOR OPERATION; HOWEVER, MODULE B NEEDED MORE MIST ELIMINATOR TRAYS.

DURING THE MONTH, THE THICKENER WAS DRAINED FOR REPAIRS THAT WERE EXPECTED TO BE COMPLETED BY THE MIDDLE OF SEPTEMBER.

9/81 SYSTEM .0 .0 .0 .0 720 677 0 85.4

#### ** PROBLEMS/SOLUTIONS/COMMENTS

MIST ELIMINATOR INSTALLATION WAS COMPLETED ON MODULES A,C, AND D BUT WAS CONTINUING ON MODULE B.

THE THICKENER WAS REFILLED AFTER WORK WAS COMPLETED TO REPAIR LEAKS IN THE BASE. AFTER REFILLING, MORE LEAKS WERE FOUND SO THE THICKENER WAS DRAINED AGAIN.

10/81	A	15.4	15.4	15.5	15.3				
	В	.0	. 0	. 0	.0				
	С	14.1	13.8	13.9	13.7				
	D	12.8	12.2	12.2	12.1				
	SYSTEM	14.1	13.8	13.9	13.7	744	739	102	81.9

#### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING OCTOBER INSTRUMENTATION PROBLEMS WITH MODULES A, C AND D WERE ENCOUNTERED.

11/81	A	91.9	91.9	91.9	91.9				
	В	. 0	.0	.0	. 0				
	С	68.5	68.4	68.4	68.4				
	D	78.8	78.6	78.6	78.6				
	SYSTEM	79.6	79.5	79.6	79.6	720	72 <b>0</b>	573	90.8
12/81	A	79.5	79.4	79.4	79.4				
	В	.0	.0	.0	.0				
	С	89.6	89.4	89.4	89.4				
	D	83.6	83.5	83.5	83.5				
	SYSTEM	84.2	84.1	84.1	84.1	744	744	626	88.5

# ** PROBLEMS/SOLUTIONS/COMMENTS

REPLACEMENT PARTS NEEDED FOR MODULE B KEPT THE MODULE OFF-LINE THROUGH THE FOURTH QUARTER.

DURING NOVEMBER AND DECEMBER PLUGGING IN THE LIMESTONE BALL MILL WAS A MINOR PROBLEM.

1/82 A	82.0	82.5	82.8	81.8				
₿	.0	.0	.0	.0				
С	87.4	87.5	87.8	86.7				
D	89.8	90.3	90.6	89.5				
SYS	TEM 86.4	86.8	65.3	86. <b>0</b>	744	737	640	84.2

# ** PROBLEMS/SOLUTIONS/COMMENTS

DURING JANUARY THE MIST ELIMINATORS WERE CLEANED WEEKLY.

ROCKS IN THE LIMESTONE HAS CAUSED PLUGGING OF THE BALL MILL. THE SUPPLIER IS WORKING ON THE PROBLEM.

UTILITY FGD SURVEY: OCTOBER 1983 - SEPTEMBER 1984

COLORADO UTE ELECTRIC: CRAIG 1 (CONT.)

FKIOD	MODULE AV	AILABILIT	Y OPERABILITY	RELIABILITY	CE DATA UTILIZATION %	REMOVAL 02 PART.	PER HOURS	BOILER	FGD HOURS	CAP. FACTOR
	<i>*</i>		THE UTILITY IS	WAITING FOR	PARTS TO MAKE					ULE B.
2/82	A	72.9	73.1	73.9	72.8					
	_			A 4	Α 1					
	С	88.8	89.1	90.0	88.7					
	D	65.3	65.5	66.2	65.2					
	SYSTEM	76.5	89.1 65.5 76.6	76.3	76.3		672	669	513	83.6
	** PROBLE	MS/SOLUTIO	ONS/COMMENTS							
			MODULE B WAS R STARTED UP.	EPAIRED DURI	NG THE MONTH A	ND IS IN	THE PRO	CESS O	F BEING	,
			DURING FEBRUAR LUBRICATION SY		IERE ENCOUNTERE	ואד אדוש ס	E LIMES	TONE BA	ALL MIL	.L
3/82	A		40.9							
	В	85.4	85.4 85.1	86.5	85.2					
	C		85.1	86.2	84.9					
	D	79.7	79.7	80.7	79.5					
	SYSTEM	96.9	97.1	98.3	96.8		744	742	720	80.2
	** PROBLE	MS/SOLUTI	ONS/COMMENTS							
		I	DURING MARCH M	ODULE A WAS	DOWN 428 HOURS	FOR CLEAN	NING.			
4/82		46.9		49.2						
	В	70.7	71.0	74.2 79.7	70.6					
	C	76.1	76.3	79.7	75.8					
	D	20.8	20.8							
	SYSTEM	71.5	71.7	75.0	71.3		720	715	513	82.7
	** PROBLE	MS/SOLUTIO	ONS/COMMENTS							
		I	DURING APRIL P	ROBLEMS WERE	ENCOUNTERED W	ITH THE S	JPERNAT	E PUMPS	5.	
5/82	A	22.7	56.4	64.9	22.6					
	В	29.2	72.6	83.6	29.1					
	С	29.2	72.5 .0	83.4	29.0					
	D	.0	. 0	.0	.0					
	SYSTEM	27.0	67.2	77.3	26.9		744	298	200	25.6
	** PROBLE	MS/SOLUTI	ONS/COMMENTS							
			DURING MAY THE THE FGD SYSTEM	UNIT WAS OF	F-LINE FOR THR PLIANCE PRIOR T	EE WEEKS	FOR A S	CHEDULI	ED OUTA	GE.
6/82	A	. 0	.0	.0	.0					
	В	58.2	58.1	58.1	58.1					
	С	58.5	58.2	58.2	58.2					
	D	. 0	.0	.0	.0					
	SYSTEM	38.9	38.8	38.8	38.8		720	72 <b>0</b>	279	77.3
	** PROBLE	MS/SOLUTIO	ONS/COMMENTS							
			AT THE BEGINNI	NG OF JUNE,	ALL MODULES WE	RE DOWN DE	UE TO F	AULTY	PIPING	ОИ
		•	INE SUPERNATE	OTOTOTION MILEC	KEI AEKED					
		•			INE THE REST O		TH DUE	TO LIN	ER PROE	BLEMS.
7/82	A	•	MODULES A AND	D WERE OFF-L	INE THE REST O		TH DUE	TO LIN	ER PROE	BLEMS.
7/82	A B	1					TH DUE	TO LIN	ER PROE	BLEMS.

PERIOD			OPERABILITY			502	PART.	HOURS	HOURS		
	D	.0	.0 16.9	.0	.0				720	121	62.8
	** PROBL	EMS/SOLUTIO	NS/COMMENTS								
		r	OURING JULY AS	SORBER LINE	R REPAIRS CON	TRIBU	TED TO	MODULA	AR OUTAG	SES.	
		1	1AJOR DEMISTER	REPAIRS AL	SO RESULTED I	N DOM	N TIME	DURIN	JULY.		
8/82	A	68.1	69.7	77.1	68.0						
	В	5.1	5.2	5.7	5.0						
	С	.0	.0	.0	.0						
	a	.0	.0	.0	.0						
	-	24.4	25.0	27.6	24.3			76.6	725	101	44.0
	3131611	24.4	25.0	27.6	24.3			/44	125	101	64.0
	** PROBL	EMS/SOLUTIO	ONS/COMMENTS								
		•	10DULES C AND STRIKE PREVEN ALSO CONTRIBU	TED COMPLETI	ON OF THESE R						
			ODULE B EXPER				URING	AUGUST	. THEY	WERE	
9/82		3.5	3.7	3.6	3.5						
	В	84.2	89.2	88.2	84.0						
	С	.0	.0	.0	.0						
	D	.0	.0	.0	.0						
	SYSTEM	29.2	31.0	30.6	29.2			720	678	210	68.5
	** PROBL	EMS/SOLUTIO	ONS/COMMENTS								
			DURING SEPTEM ABSORBER LINE		C AND D WERE	DOWN	ITIAWA	NG COMI	PLETION	OF THE	Ξ
		1	10DULE A WAS I	ONN DURING	THE MONTH FOR	DEMI	STER W	ASH MOI	DIFICAT:	IONS.	
10/82	A	61.8	61.7	61.7 61.6	61.7						
	В	61.8	61.6	61.6	61.6						
	С	.0	.0	.0	. 0						
	D	. 0	.0	. 0	.0						
			• •		• •						78.1
	SYSTEM	41.2	41.1	41.1	41.1			744	744	306	,
					41.1			744	744	306	75.1
		EMS/SOLUTIO	DNS/COMMENTS	41.1		SER FO	R DFMI				
		EMS/SOLUTIO		41.1  B WERE DOWN  D REMAINED	DURING OCTOB			STER RI	EPAIRS /	AND CLI	EANING.
11/02	** PROBL	EMS/SOLUTIO	ONS/COMMENTS MODULES A AND MODULES C AND THE ABSORBER	41.1 B WERE DOWN D REMAINED LINER.	DURING OCTOB			STER RI	EPAIRS /	AND CLI	EANING
1/82	** PROBL	EMS/SOLUTION PROPERTY OF THE P	ONS/COMMENTS  10DULES A AND 10DULES C AND THE ABSORBER  77.1	41.1  B WERE DOWN  D REMAINED LINER.  90.1	DURING OCTOB OUT OF SERVIC 63.1			STER RI	EPAIRS /	AND CLI	EANING
11/82	** PROBL	EMS/SOLUTION N	ONS/COMMENTS  10DULES A AND 10DULES C AND THE ABSORBER  77.1 67.6	41.1  B WERE DOWN  D REMAINED LINER.  90.1 79.0	DURING OCTOB OUT OF SERVIC 63.1 55.3			STER RI	EPAIRS /	AND CLI	EANING
11/82	** PROBL  A B C	EMS/SOLUTION  63.2 55.4 .0	DNS/COMMENTS  HODULES A AND HODULES C AND THE ABSORBER  77.1 67.6 .0	41.1  B WERE DOWN  D REMAINED LINER.  90.1 79.0 .0	DURING OCTOB OUT OF SERVIC 63.1 55.3 .0			STER RI	EPAIRS /	AND CLI	EANING
11/82	** PROBL	EMS/SOLUTION N	ONS/COMMENTS  10DULES A AND 10DULES C AND THE ABSORBER  77.1 67.6	41.1  B WERE DOWN  D REMAINED LINER.  90.1 79.0	DURING OCTOB OUT OF SERVIC 63.1 55.3			STER RI	EPAIRS A	AND CLI	EANING

# ** PROBLEMS/SOLUTIONS/COMMENTS

MODULES C AND D REMAINED OUT OF SERVICE DURING NOVEMBER AWAITING ABSORBER LINER REPAIRS.

THE UNIT WAS DOWN FOR PART OF THE MONTH DUE TO A SCHEDULED OUTAGE.

12/82 A 100.0 100.0 100.0 100.0

ERIOD	MODULE				NCE DATA UTILIZATION	% RE	MOVAL	PER	BOILER HOURS		
	В	7.7	7.5	7.5	7.5						
	С	. 0		.0	. 0						
	D SYSTEM	.0 35.9	.0	.0 35.8	.0			766	744	24.4	71 7
		35.9 SLEMS/SOLUTIO		33.0	33.0			/44	744	200	/1.3
	** PROE			D 11505 DOING	****	101711					
		۲			THE ENTIRE M						
1/83		95.8		98.1							
	В С	.0 .0	.0	. 0 . <b>0</b>	.0						
	D	.0	. ŏ	.0	.0						
	SYSTEM	31.9		32.7				744	743	237	68.5
	** PROE	LEMS/SOLUTIO	NS/COMMENTS								
		M	ODULES B, C	AND D WERE DO	OWN DURING JA	NUARY	FOR A	SORBER	LINER	REPAIR	ls.
2/83		57.2		59.1	57.2						
	B C	.0	.0	.0	.0						
	D	.0 88.1	.0 45.5	.0 46.7	.0 45.2						
		48.4	34.3	35.3	34.2			672	668	230	63.0
	** PROB	LEMS/SOLUTIO	NS/COMMENTS								
		M	ODULE A WAS	DOWN DURING I	FEBRUARY FOR	PREVE	TIVE 1	1AINTE	NANCE.		
		м	ODULE B WAS	DOWN DURING F	FEBRUARY FOR	ABSORE	BER LIN	IER REF	PAIRS.		
		м	ODULE C WAS I	DOWN DURING	THE MONTH FOR	REPA	IRS ON	THE BO	OSTER F	AN LUE	E SET.
			ODULE D WAS A		RING FEBRUARY	BUT I	NI TON	SERVIC	E. THE	UTILI	TY WAS
3/83		.0	.0	.0 79.5	.0						
	B C	67.1 .0	.0	79.5 .0	67.1						
	0	71.0	81.1	84.2	.0 71.0						
	SYSTEM	46.1		54.6				744	652	343	61.7
	** PROB	LEMS/SOLUTIO	NS/COMMENTS								
		M	ODULE A WAS D	OOWN DURING 1	MARCH DUE TO	PROBLE	EMS WIT	TH SCAL	E BUILD	)-UP 01	THE
		R M	ECYCLE PUMP F	PROBLEMS ALSO	CONTRIBUTED	סס סד	NIT NWC	1E FOR	MODULE	A DURI	NG THE
		M D	ODULE C AWAIT URING MARCH.	TED COMPLETIO	ON OF WORK ON	THE 3	INTERF A	CE WAS	H SPRAY	HEADE	R
4/83	A	.0	.0	. 0	.0						
	В	10.3	9.3	9.7	9.3						
	C D	.0	.0	.0	.0						
	SYSTEM	92.4 33.8	89.4 32.9	93.4	89.2						:
	2.2.411	33.0	36.7	34.3	32.8			720	718	236	73.6

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

#### ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE A WAS DOWN DURING THE MONTH TO ALLOW FOR WORK ON A RECYCLE PUMP.

A CLEANING OF THE INLET DUCTWORK ALSO CAUSED DOWN TIME FOR MODULE A DURING APRIL.

MODULE B WAS OUT OF SERVICE FOR MIST ELIMINATOR CLEANING.

MODULE C WAS DOWN SO THAT REPAIRS COULD BE MADE TO A SECTION OF A WASH SPRAY HEADER.

5/83	A	.0	.0	.0	.0				
	В	64.8	66.9	79.8	64.8				
	С	.0	.0	.0	.0				
	D	32.8	33.7	40.2	32.7				
	SYSTEM	32.5	33.5	40.0	32.5	744	721	242	70.7

# ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE A WAS DOWN DURING THE MONTH FOR RECYCLE PUMP REPAIRS.

MODULE C WAS OUT OF SERVICE SO THAT REPAIRS COULD BE MADE ON A WASH-SPRAY HEADER.

6/83	A	31.1	4.6	5.1	4.4				
	В	57.0	31.1	34.5	30.3				
	С	.0	.0	.0	.0				
	0	66.7	68.4	75.8	66.7				
	SYSTEM	51.6	34.7	38.5	33.8	720	701	243	68.4

# ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE A WAS DOWN DURING THE FIRST PART OF JUNE DUE TO PROBLEMS WITH RECYCLE PUMP BEARINGS.

MODULE C WAS DOWN FOR THE ENTIRE MONTH OF JUNE DUE TO PROBLEMS WITH THE BOOSTER FAN BLADE PITCH CONTROL.

7/83	A	82.9	82.9	100.0	82.9				
	В	85. <b>3</b>	56. <b>3</b>	71.5	56.3				
	С	50.5	34.4	43.7	34.4				
	D	.0	.0		. 0				
	SYSTEM	72.9	57.9	73.5	57.8	744	743	430	74.7

# ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE C WAS OUT OF SERVICE DURING THE FIRST 12 DAYS OF JULY DUE TO MIST ELIMINATOR HEADER PROBLEMS.

MODULE D WAS OUT OF SERVICE UNTIL JULY 25 DUE TO RECYCLE PUMP PROBLEMS.

8/83	A	96.0	96.1	96.5	96.0				
	В	.0	.0		.0				
	С	100.0	100.0	100.0	100.0				
	D	91.0	8.5	8.5	8.5				
	SYSTEM	95.7	68.2	68.5	68.1	744	743	507	
9/83	A	94.5	94.8	96.3	94.5				
	В	48.4	51.7	52.6	51.6				
	С	56.5	43.6	44.3	43.5				
	D	.0	.0		. 0				
	SYSTEM	66.5	63.4	64.4	63.2	720	718	455	75.6

UTILITY FGD SURVEY: OCTOBER 1983 - SEPTEMBER 1984

COLORADO UTE ELECTRIC: CRAIG 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

#### ** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURING AUGUST AND SEPTEMBER.

10/83	A	67.7	100.0	100.0	67.7
	В	22.3	65.2	65.1	44.1
	С	. 0	.0		.0
	D	53.0	21.9	21.8	14.8
	SYSTEM	47.7	62.4	62.3	42.2

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS OUT OF SERVICE FROM OCTOBER 21 THROUGH THE END OF THE MONTH FOR AN ANNUAL MAINTENANCE OUTAGE.

744 503 314 82.0

11/83	A	.0	. 0	.0		
	В	46.7	96.0	46.7		
	С	39.3	80.9	39.3		
	D	.0		.0		
	SYSTEM	28.7	59.0	28.7	720	206

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE ANNUAL MAINTENANCE OUTAGE WHICH BEGAN IN OCTOBER CONTINUED THROUGH NOVEMBER 12.

THE UTILITY REPORTED PROBLEMS WITH A CIRCULATING WATER PUMP FROM NOVEMBER 13 TO NOVEMBER 15, 1983. THE UNIT WAS BROUGHT DOWN DURING THIS PERIOD.

MODULES A AND C WERE DOWN DURING PART OF NOVEMBER DUE TO ABSORBER GAS AND LIQUID SIDE EQUIPMENT PROBLEMS.

THE UNIT WAS PLACED BACK IN SERVICE ON NOVEMBER 16.

12/83	A	.0	.0		. 0				
	В	99.2	100.0	100.0	99.2				
	С	99.2	100.0	100.0	99.2				
	۵	15.7	15.9	100.0	15.7				
	SYSTEM	71.4	72.0	100.0	71.4	744	736	531	98.9

# ** PROBLEMS/SOLUTIONS/COMMENTS

MODULES A AND D EXPERIENCED PROBLEMS WITH ABSORBER LIQUID SIDE EQUIPMENT DURING DECEMBER.

1/84	A	.0	.0		.0			
	В	100.0	100.0	100.0	100.0			
	С	32.5	32.5	32.5	32.5			
	D	96.2	96.2	96.2	96.2			
	SYSTEM	76.3	76.3	76.3	76.3	744	744	567

#### ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE A WAS DOWN FOR LIQUID SIDE EQUIPMENT PROBLEMS DURING JANUARY.

MODULE C WAS DOWN FOR LIQUID AND GAS SIDE EQUIPMENT PROBLEMS.

2/84	SYSTEM	696
3/84	SYSTEM	744
4/84	SYSTEM	720

PERFORMANCE DATA								
	_	-						
OPERABILITY	RELIABILITY	UTILIZATION	% RE	MOVAL	PER	BOILER	FGD	CAP.
			502	PART	HOURS	HOURS	HOURS	FACTOR
			JUL	10001				
		_	OPERABILITY RELIABILITY UTILIZATION	OPERABILITY RELIABILITY UTILIZATION % RE	OPERABILITY RELIABILITY UTILIZATION % REMOVAL	OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER	OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER	OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD SO2 PART. HOURS HOURS

#### ** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE PERIOD OF FEBRUARY THROUGH APRIL 1984.

5/84	A	99.2	83.7	99.9	83.1			
	В	.0	.0		.0			
	С	99.3	100.0	100.0	99.3			
	D	98.6	99.2	99.2	98.6			
	SYSTEM	99.0	94.3	99.7	93.7	744	739	697
6/84	A	100.0	100.0	100.0	100.0			
	В	28.3	.0	.0	.0			
	С	100.0	76.5	103.4	76.5			
	D	100.0	89.0	100.0	89.0			
	SYSTEM	100.0	88.5	100.0	88.5	720	720	637
7/84	A	100.0	78.8	100.0	100.0			
	В	41.9	21.3	93.1	27.0			
	С	91.5	53.7	100.0	68.1			
	D	99.9	78.7	100.0	99.9			
	SYSTEM	100.0	77.5	100.0	98.3	744	744	732
8/84	A	84.3	80.1	100.0	80.1			
	В	68.4	67.5	147.8	67.5			
	С	100.0	95.6	95.6	95.6			
	D	29.0	19.4		19.4			
	SYSTEM	93.9	87.5	100.0	87.5	744	744	651

# ** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE REPORTED DURING THE PERIOD OF MAY THROUGH AUGUST 1984.

9/84 SYSTEM 720

#### ** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR SEPTEMBER 1984.

# SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

______ COLORADO UTE ELECTRIC COMPANY NAME CRAIG PLANT NAME UNIT NUMBER CRAIG CITY COLORADO STATE PARTICULATE EMISSION LIMITATION - NG/J 43. ( .100 LB/MMBTU)
SO2 EMISSION LIMITATION - NG/J 172. ( .400 LB/MMBTU)
NOX EMISSION LIMITATION - NG/J 301. ( .700 LB/MMBTU)
NET PLANT GENERATING CAPACITY - MW 900
GROSS UNIT GENERATING CAPACITY - MW 455
NET UNIT GENERATING CAPACITY W/FGD - MW 400
NET UNIT GENERATING CAPACITY WO/FGD - MW 406
EQUIVALENT SCRUEBED CAPACITY - MW 455 REGULATORY CLASSIFICATION С ** UNIT DATA - BOILER AND STACK BABCOCK & WILCOX BOILER SUPPLIER PULVERIZED COAL BASE BOILER TYPE BOILER SERVICE LOAD

DESIGN BOILER FLUE GAS FLOW - CU.M/S

BOILER FLUE GAS TEMPERATURE - C

STACK HEIGHT - M

STACK SHELL

STACK TOP DIAMETER - M

BASE

(1530600 ACFM)

(250 F)

(250 F)

(600 FT)

CONCRETE

STACK TOP DIAMETER - M

10.9

(35.8 FT) ** FUEL DATA FUEL TYPE COAL SUBBITUMINOUS FUEL GRADE AVERAGE HEAT CONTENT - J/G 23260. ( 10000 BTU/LB) RANGE- HEAT CONTENT - BTU/LB 8.00 9100-10300 AVERAGE ASH CONTENT % ***** 16.00 RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - %
RANGE MOISTURE CONTENT - %
AVERAGE SULFUR CONTENT % 16.00 .45 0.4-0.5 RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - %
RANGE CHLORIDE CONTENT - % ***** RANGE CHLORIDE CONTENT % 0.00-0.02 *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER TYPE NONE ** ESP NUMBER NUMBER OF SPARES 0 TYFF HOT SIDE SUPPLIER BELCO INLET FLUE GAS CAPACITY - CU.M/S
THLET FLUE GAS TEMPERATURE - C 1392.1 (2950000 ACFM) 398.9 (750 F) .7 (3. IN-H20) 99.9 INLET FLUE GAS TEMPERATURE - C PRESSURE DROP - KPA PARTICLE REMOVAL EFFICENCY - % ** PARTICLE SCRUBBER NUMBER 0 GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL N/A LINER GENERIC MATERIAL N/A LINER SPECIFIC MATERIAL N/A GAS CONTACTING DEVICE TYPE N/A

*** FGD SYSTEM

SPECIFIC TYPE

```
** GENERAL DATA
                                               THROWAWAY PRODUCT
   SALEABLE PRODUCT/THROWAWAY PRODUCT
   SO2 REMOVAL MODE
                                               WET SCRUBBING
                                               LIMESTONE
   PROCESS TYPE
   PROCESS ADDITIVES
                                               NONE
   SYSTEM SUPPLIER
                                               PEABODY PROCESS SYSTEMS
   A-E FIRM
                                               STEARNS-ROGER
   DEVELOPMENT LEVEL
                                               FULL SCALE
   NEW/RETROFIT
                                               NEW
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.80
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                  85.00
   ENERGY CONSUMPTION - %
   CURRENT STATUS
                                                1
   COMMERCIAL START-UP
                                                5/80
   INITIAL START-UP
                                               12/79
   CONTRACT AWARDED
                                                5/77
** DESIGN AND OPERATING PARAMETERS
   DESIGN COAL SULFER CONTENT - X
                                                     . 96
    DESIGN COAL HEAT CONTENT - J/G
                                               22329.6
                                                               ( 9600 BTU/LB)
    DESIGN COAL ASH CONTENT - %
                                                  11.60
    DESIGN MOISTURE CONTENT - %
                                                  15.30
    DESIGN CHLORIDE CONTENT - %
                                                    .10
    SPACE REQUIREMENTS - SQ M
                                               12140.2
                                                               ( 130680 SQ FT)
    OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                 264.0
** QUENCHER/PRESATURATOR
    NUMBER
    TYPE
                                               QUENCH DUCT
    SUPPLIER
                                               PEABODY PROCESS SYSTEMS
    INLET GAS FLOW - CU. M/S
                                                 217.07
                                                           ( 460000 ACFM)
    INLET GAS TEMPERATURE - C
                                                 121.1
                                                               ( 250 F)
                                                              ( 1.0 IN-H20)
    PRESSURE DROP - KPA
                                                    . 2
                                                              ( 500 GPM).
( 1.1 GAL/1000 ACFM)
    LIQUID RECIRCULATION RATE - LITERS/S
                                                   31.
    L/G RATIO - L/CU. M
                                                     .1
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               HIGH ALLOY
                                               NICKEL BASE/CHROMIUM-IRON-MOLYBDENUM
    CONSTRUCTION MATERIAL SPECIFIC TYPE
** ABSORBER
    NUMBER
                                                 4
    NUMBER OF SPARES
                                                1
                                                SPRAY TOWER
    GENERIC TYPE
    SPECIFIC TYPE
                                               OPEN COUNTERCURRENT SPRAY
    TRADE NAME/COMMON TYPE
                                               N/A
                                               PEABODY PROCESS SYSTEMS
    SUPPLIER
    DIMENSIONS - FT
                                               32.0 DIA X 52.5
    SHELL GENERIC MATERIAL
                                               CARBON STEEL
    SHELL SPECIFIC MATERIAL
                                               AISI 1110
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                               N/A
    LINER GENERIC MATERIAL
                                               ORGANIC (SPRAY ZONE); GLASS FLAKE-FILLED POLYEST
                                               NATURAL RUBBER
    LINER SPECIFIC MATERIAL
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                               BLACK NATURAL RUBBER
    GAS CONTACTING DEVICE TYPE
                                               NONE
    NUMBER OF CONTACTING ZONES
                                                 4
    LIQUID RECIRCULATION RATE - LITER/S
                                                 1512.
                                                               (24000 GPM)
                                                               ( 52.2 GAL/1000 ACF)
    L/G RATIO - L/CU.M
                                                    7.0
    GAS-SIDE PRESSURE DROP - KPA
                                                               ( 1.5 IN-H20)
                                                    .4
    SUPERFICAL GAS VELOCITY - M/SEC
                                                   3.0
                                                              ( 10.0 FT/S)
    INLET GAS FLOW - CU. M/S
                                                  217.07
                                                               ( 460000 ACFM)
    INLET GAS TEMPERATURE - C
                                                               ( 250 F)
                                                 121.1
    SO2 REMOVAL EFFICIENCY - %
                                                  85.0
    PARTICLE REMOVAL EFFICENCY - %
                                                  50.0
** MIST ELIMINATOR
   PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                               PRIMARY COLLECTOR
    NUMBER PER SYSTEM
                                                 4
   NUMBER OF SPARES PER SYSTEM
                                                1
   NUMBER PER MODULE
                                               IMPINGEMENT
   GENERIC TYPE
```

BAFFLE

```
CLOSED VANE
   TRADE NAME/COMMON TYPE
                                              HORIZONTAL
   CONFIGURATION
                                                 1
   NUMBER OF STAGES
   NUMBER OF PASSES PER STAGE
                                                  4
                                                           ( 5.0 FT)
   FREEBOARD DISTANCE - M
                                                 1.52
                                                            ( 1.20 IN)
                                                 3.0
   DISTANCE BETWEEN VANES - CM
   VANE ANGLES - DEGREES
                                                45
                                                   .2
                                                            ( 1.0 IN-H20)
   PRESSURE DROP - KPA
   SUPERFICAL GAS VELOCITY - M/S
                                                 3.0
                                                            ( 10.0 FT/S)
                                             ORGANIC
   CONSTRUCTION MATERIAL GENERIC TYPE
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                             POLYPHENYLENE
                                             RAW WATER
   WASH WATER SOURCE
   WASH FREQUENCY
                                             CONTINUOUS
                                                           ( 100 GAL/MIN)
   WASH RATE - L/S
                                                 6.3
** REHEATER
                                               4
   NUMBER
   NUMBER OF SPARES
                                               1
   NUMBER PER MODULE
                                               1
                                             BYPASS
   GENERIC TYPE
   SPECIFIC TYPE
                                             COLD SIDE
   TRADE NAME/COMMON TYPE
                                             N/A
    LOCATION
                                              OUTLET DUCT BETWEEN ME & OUTLET DAMPER
                                              23.0
   PERCENT GAS BYPASSED - AVG
   TEMPERATURE INCREASE - C
                                                27.8
                                                           ( 50 F)
                                                           ( 413000 ACFM)
   INLET FLUE GAS FLOW RATE - CU. M/S
                                              194.89
43.3
   INLET FLUE GAS TEMPERATURE C
                                                            ( 110 F)
                                              302.02 ( 640000 ACFM)
73.9 ( 165 F)
   OUTLET FLUE GAS FLOW RATE - CU. M/S
   OUTLET FLUE GAS TEMPERATURE - C
CONSTRUCTION MATERIAL GENERIC TYPE
                                           STAINLESS STEEL AUSTENITIC
   CONSTRUCTION MATERIAL SPECIFIC TYPE
** FANS
   NUMBER
                                               4
   NUMBER OF SPARES
                                              0
   DESIGN
                                              AXIAL
   SUPPLIER
                                              BUFFALO FORGE
   FUNCTION
                                              INDIRECT REHEAT
   APPLICATION
                                              N/A
    SERVICE
                                            46.03 ( 97545 ACFM)
CARBON STEEL
   FLUE GAS FLOW RATE - CU.M/S
   CONSTRUCTION MATERIAL GENERIC TYPE
** FANS
   NUMBER
                                               4
   NUMBER OF SPARES
                                               1
   DESIGN
                                              AXIAL
   SUPPLIER
                                              BUFFALO FORGE
    FUNCTION
                                              BOOSTER
   APPLICATION
                                              FORCED DRAFT
    SERVICE
                                              DRY
   FLUE GAS FLOW RATE CU.M/S
                                              372.80
                                                           ( 790000 ACFM)
    FLUE GAS TEMPERATURE - C
                                                           ( 250 F)
                                               121.1
3.4
    PRESSURE DROP - KPA
                                                            (11.0 IN-H20)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                            CARBON STEEL
** DAMPERS
   NUMBER
                                              4
   GENERIC TYPE
                                              LOUVER
   SPECIFIC TYPE
                                              PARALLEL BLADE MULTILOUVER
   MANUFACTURER
                                              FORNEY ENGINEERING
   MCDULATION
                                              OPEN
   SEAL AIR FLOW - CU. M/S
                                              3.07
                                                           ( 6500 ACFM)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                            CARBON STEEL/STAINLESS STEEL
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                             ASTM A-285
   LINER GENERIC MATERIAL TYPE
                                             NONE
   LINER SPECIFIC MATERIAL TYPE
                                             N/A
** DAMPERS
   NUMBER
   GENERIC TYPE
                                              LOUVER
```

SPECIFIC TYPE
MANUFACTURER
MODULATION
SEAL AIR FLOW - CU. M/S
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

# ** DAMPERS

NUMBER
GENERIC TYPE
SPECIFIC TYPE
MANUFACTURER
MODULATION
SEAL AIR FLOW - CU. M/S
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

#### ** DAMPERS

NUMBER
GENERIC TYPE
SPECIFIC TYPE
MANUFACTURER
MODULATION
SEAL AIR FLOW ~ CU. M/S
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

#### ** DAMPERS

NUMBER
GENERIC TYPE
SPECIFIC TYPE
MANUFACTURER
MODULATION
SEAL AIR FLOW - CU. M/S
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

#### ** DAMPERS

NUMBER
GENERIC TYPE
SPECIFIC TYPE
MANUFACTURER
MODULATION
SEAL AIR FLOW - CU. M/S
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

# ** DAMPERS

NUMBER
GENERIC TYPE
SPECIFIC TYPE
MANUFACTURER
MCDULATION
SEAL AIR FLOW - CU. M/S
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

PARALLEL BLADE MULTILOUVER FORNEY ENGINEERING OPEN 3.07 ( 6500 ACFM) CARBON STEEL/STAINLESS STEEL ASTM A-285 NONE N/A

4
LOUVER
PARALLEL BLADE MULTILOUVER
FORNEY ENGINEERING
OPEN
3.07 ( 6500 ACFM)
CARBON STEEL/STAINLESS STEEL
ASTM A-285
NONE
N/A

GUILLOTINE
NR
FORNEY ENGINEERING
OPEN
.00 ( 0 ACFM)
CARBON STEEL/HIGH ALLOY
AISI 1110; NR
NONE
N/A

2
LOUVER
PARALLEL BLADE MULTILOUVER
FORNEY ENGINEERING
OPEN
.00 ( 0 ACFM)
CARBON STEEL/STAINLESS STEEL
ASTM A-285
NONE
N/A

1
LOUVER
PARALLEL BLADE MULTILOUVER
FORNEY ENGINEERING
OPEN
.00 ( 0 ACFM)
CARBON STEEL/STAINLESS STEEL
ASTM A-285
NONE
N/A

2
LOUVER
PARALLEL BLADE MULTILOUVER
FORNEY ENGINEERING
CLOSED
.00 ( 0 ACFM)
CARBON STEEL/STAINLESS STEEL
ASTM A-285
NONE
N/A

COLORADO UTE ELECTRIC: CRAIG 2 (CONT.)

**	DUCTWORK LOCATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	INLET TO QUENCH CARBON STEEL AISI 1110 NONE N/A
**	DUCTWORK LOCATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	OUTLET TO DAMPER CARBON STEEL AISI 1110 ORGANIC GLASS FLAKE-FILLED POLYESTER
**	DUCTWORK LOCATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	DAMPER TO STACK CARBON STEEL AISI 1110 NONE N/A
**	DUCTWORK LOCATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	BYPASS CARBON STEEL AISI 1110 NONE N/A
**	REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE DEVICE TYPE MANUFACTURER NUMBER NUMBER OF SPARES FULL LOAD DRY FEED CAPACITY - M.TONS/HR PRODUCT QUALITY - % SOLIDS	WET BALL MILL COMPARTMENTED NR KENNEDY VAN SAUN 1 0 9.1 ( 10 TPH) 35.0
**	TANKS SERVICE ABSORBER RECYCLE REAGENT PREP PRODUCT THICKENER OVERFLOW CLASSIFIER OVERFLOW FLOCCULANT WASTE SLURRY BLEED	NUMBER
**	PUMPS SERVICE RAH WATER RECLAIM SUMP POND COCLING TOWER BLOWDOWN BOOSTER ABSORBER RECIRCULATION WASH SLURRY SUPERNATANT THICKENER UNDERFLOW POLYELECTROLYTE WASTE SLURRY MILL RECIRCULATION LIMESTONE SLURRY FEED	NUMBER  2 7 1 2 8 8 8 2 2 1 2 2
**	SOLIDS CONCENTRATING/DEWATERING DEVICE NUMBER NUMBER OF SPARES DIMENSIONS FT CAPACITY	CENTRIFUGE  1 1 3.0 DIA X 6.0 126 GPM

SHELL GENERIC MATERIAL TYPE HIGH ALLOY NICKEL BASE/CHROMIUM-IRON-MOLYBDENUM SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A BELT GENERIC MATERIAL TYPE N/A BELT SPECIFIC MATERIAL TYPE N/A FEED STREAM SOURCE THICKENER UNDERFLOW FEED STREAM CHARACTERISTICS 35% SOLIDS OUTLET STREAM CHARACTERISTICS 60% SOLIDS OVERFLOW STREAM CHARACTERISTICS 60 GPM **OUTLET STREAM DISPOSITION** LANDETIL OVERFLOW STREAM DISPOSITION TO WASTE SUMP & THEN TO THICKENER ** SOLIDS CONCENTRATING/DEWATERING DEVICE THICKENER NUMBER 1 NUMBER OF SPARES n CONFIGURATION CENTER DRAW DIMENSIONS - FT 75.0 DIA X 15.0 SHELL GENERIC MATERIAL TYPE CARBON STEEL SHELL SPECIFIC MATERIAL TYPE AISI 1110 LINER GENERIC MATERIAL TYPE ORGANIC LINER SPECIFIC MATERIAL TYPE GLASS FLAKE-FILLED POLYESTER (WALLS); MAT-REINFO FEED STREAM SOURCE ABSORBER BLEED FEED STREAM CHARACTERISTICS 5% SOLIDS OUTLET STREAM CHARACTERISTICS 35% SOLIDS OVERFLOW STREAM CHARACTERISTICS 100 GPM, <1% SUSPENDED SOLIDS OUTLET STREAM DISPOSITION TO CENTRIFUGES OVERFLOW STREAM DISPOSITION RECYCLED TO PROCESS *** SLUDGE FULL LOAD SLUDGE QUANTITY - M.TONS/HR (DRY) 10.5 ( 11.6 TPH) MOISTURE CONTENT - % TOTAL FREE WATER 40.0 % CASO3 - DRY 22.6 % CASO4 - DRY 70.2 % CAOH2 DRY . 0 % CACO3 - DRY 2.9 % ASH - DRY. . 3 % OTHER COMPOUNDS - DRY 3.9 NONE METHOD ** DISPOSAL **NATURE** FINAL

#### ** TREATMENT

LANDETLL TYPE ON-SITE LOCATION SITE TRANSPORTATION METHOD TRUCK

#### ** PROCESS CONTROL AND INSTRUMENTATION

CHEMICAL PARAMETERS PH, SO2 CONCENTRATION PHYSICAL VARIABLES DENSITY, GAS FLOW, LIQUID FLOW CONTROL LEVELS PH 5.4, SOLIDS 12-15% MONITOR TYPE UNILOK-PH, OHMART-DENSITY, BROOKS-FLOW, DYNASCIE MONITOR LOCATION AT MODULE RECYCLE TANK PROCESS CONTROL MANNER AUTOMATIC PROCESS CHEMISTRY MODE FEEDBACK

#### ** WATER BALANCE

WATER LOOP TYPE CLOSED EVAPORATION WATER LOSS - LITER/S 17.8 ( 282 GPM) SLUDGE HYDRATION WATER LOSS - LITER/S 9 GPM) 2.1 SLUDGE INTERSTITIAL WATER LOSS - LITERS/S 33 GPM ) POND SEEPAGE/RUNOFF WATER LOSS - LITERS/S 0 EFFLUENT WATER LOSS - LITERS/S .0 0 GPM) RECEIVING WATER STREAM N/A LITERS/S 20.2 ( 321 GPM) MAKEUP WATER ADDITION COOLING TOWER BLOWDOWN SOURCE OF MAKEUP WATER

COLORADO UTE ELECTRIC: CRAIG 2 (CONT.)

** CHEMICALS AND CONSUMPTION FUNCTION NAME PRINCIPAL CONSTITUENT CONSUMPTION UTILIZATION - % POINT OF ADDITION	ABSORBENT LIMESTONE CACO3 7000 LB/HR 75.0 BALL MILL
** FGD SPARE CAPACITY INDICES ABSORBER % MIST ELIMINATOR - % REHEATER - % BALL MILL - % EFFLUENT HOLD TANK - % THICKENER - % CENTRIFUGE - %	33.3 33.3 .0 33.3 .0 50.0
** FGD SPARE COMPONENT INDICES ABSORBER	1.0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

7/79 SYSTEM

7/44

8/79 SYSTEM

720

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM AT CRAIG 2 WAS UNDERGOING TESTING IN JULY. INITIAL TESTING WITH THE SYSTEM OPERATING ON FLUE GAS TOOK PLACE IN AUGUST 1979. COMMERCIAL OPERATIONS ARE SCHEDULED FOR NOVEMBER 1979.

10/79	SYSTEM	744
11/79	SYSTEM	720
12/79	SYSTEM	744

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE CRAIG 2 SCRUBBING SYSTEM COMMENCED INITIAL OPERATION OFFICIALLY IN DECEMBER 1979.

THE SYSTEM WAS TAKEN OUT OF SERVICE ON DECEMBER 3 FOR INSPECTION AND SCHEDULED MAINTENANCE. THE FINE SCREEN ON THE TURBINE THROTTLE VALVE WAS REMOVED AND CLEANED. THE BOILER WAS PUT BACK ON LINE ON DECEMBER 9 AT FULL LOAD. THE FGD SYSTEM WAS PUT BACK ON LINE ON DECEMBER 19. SHAKEDOWN OPERATIONS ARE CONTINUING.

1/80	SYSTEM	744
2/80	SYSTEM	696
3/80	SYSTEM	744

# ** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER WAS DOWN AT THE END OF THE PERIOD DUE TO TURBINE RELATED PROBLEMS.

WHEN FULL LOAD OPERATIONS WERE ATTEMPTED CONTROL PROBLEMS WERE ENCOUNTERED WITH THE SCRUBBER.

720

CDLORADO UTE ELECTRIC: CRAIG 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

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PROBLEMS WITH OPENING/CLOSING THE BYPASS DAMPER HAVE BEEN ENCOUNTERED. LARGER OPERATORS ARE BEING TESTED THAT MAY SOLVE THE PROBLEM.

4/80 SYSTEM

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM IS STILL IN THE STARTUP PHASE OF OPERATIONS. TESTING IS BEING PERFORMED ON THE SYSTEM, BUT THERE HAS BEEN NO OPERATIONAL DATA REPORTED.

	SYSTEM	52.6	38.3	39.5	34.0	640	661	253	76.8
	D	30.0	18.0	18.6	16.0				
	С	47.0	37.2	38.4	33.1				
	В	42.5	32.1	33.1	28.5				
5/80	A	38.4	27.5	28.4	24.5				

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE CRAIG 2 UNIT (BOILER AND SCRUBBER) COMMENCED COMMERCIAL OPERATION ON MAY 4, 1980.

NOTE: THIS SYSTEM EFFECTIVELY HAS ONE SPARE MODULE SO THAT ONLY THREE ARE CURRENTLY NEEDED AT FULL LOAD TO MAINTAIN COMPLIANCE WITH SO2 EMISSION REGULATIONS. WHEN THE CURRENT LOW SULFUR COAL SOURCE IS EXHAUSTED (SEVERAL YEARS FROM NOW) GREATER SCRUBBING CAPACITY WILL BE REQUIRED SO THAT THERE WILL NO LONGER BE AN ENTIRE MODULE SET ASIDE AS A SPARE DURING FULL LOAD BOILER OPERATIONS. THE "SYSTEM" DEPENDABILITY FACTORS WILL BE BASED ON THREE MODULES UNTIL THE CURRENT COAL SOURCE IS EXHAUSTED.

6/80	A	47.6	41.2	42.0	37.9				
	В	53.9	48.0	48.9	44.2				
	С	61.1	55.8	56.9	51.4				
	D	34.6	27.0	27.5	24.9				
	SYSTEM	65.7	57.3	58.4	52.8	720	663	380	68.5

# ** PROBLEMS/SOLUTIONS/COMMENTS

DURING MAY AND JUNE, PROBLEMS WERE ENCOUNTERED WITH PLUGGING OF THE ABSORBER SPRAY NOZZLES.

A PROBLEM WAS ALSO ENCOUNTERED DURING INITIATION OF COMMERCIAL OPERATION WITH A HIGH PH LEVEL IN THE THICKENER UNDERFLOW.

THE SCRUBBING SYSTEM IS STILL UNDERGOING SHAKEDOWN OPERATIONS.

7/80	A	59.1	51.0	51.7	43.8				
	В	61.8	54.1	54.9	46.5				
	С	37.6	26.0	26.3	22.3				
	D	43.7	33.0	33.5	28.4				
	SYSTEM	67.4	54.7	55.5	47.0	744	640	350	65.8

# ** PROBLEMS/SOLUTIONS/COMMENTS

DURING JULY, FGD OUTAGE TIME WAS CAUSED BY PLUGGED ABSORBER SPRAY NOZZLES.

8/80	A	50.0	46.7	48.3	42.2				
	В	50.0	48.4	50. <b>0</b>	43.7				
	С	50.0	47.5	49.1	42.9				
	D	50.0	52.3	54.0	47.2				
	SYSTEM	66.7	65.0	67.1	58.7	744	672	327	75.6

COLORADO UTE ELECTRIC: CRAIG 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

#### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING AUGUST THE FGD SYSTEM EXPERIENCED ASSORTED MECHANICAL PROBLEMS.

SPRAY NOZZLE PLUGGING OCCURRED, CAUSING ADDITIONAL OUTAGE TIME WHICH ADDED TO THE LOW AVAILABILITY FACTOR DURING THE MONTH.

9/80	A	48.6	47.5	48.4	47.1				
	В	58.2	58.8	59.9	58.2				
	С	61.1	59.6	60.7	59.0				
	D	67.4	66.2	67.4	65.6				
	SYSTEM	78.4	77.4	78.8	76.6	720	713	552	85.2

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE SPRAY NOZZLES IN THE ABSORBER MODULE CONTINUED TO PLUG UP DURING SEPTEMBER.

10/80	A	99.5	89.4	93.7	11.9				
	В	99.5	91.5	95.8	12.2				
	С	99.5	88.4	92.6	11.8				
	D	99.5	92.5	96.8	12.4				
	SYSTEM	99.5	90.5	94.7	12.1	744	99	90	12.2

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER WAS TAKEN OFF LINE ON OCTOBER 5 FOR A FIVE WEEK SCHEDULED OUTAGE.

AN IN-LINE SPOT CHECK PERFORMED ON OCTOBER 4 INDICATED THAT THE FGD SYSTEM WAS ACHIEVING A 66.2% SO2 REMOVAL EFFICIENCY. THE STACK OPACITY WAS MEASURED AT 5.7%.

A	69.4	61.7	66 a <b>0</b>	27.5			
В	. 0	.0	.0	.0			
С	70.8	71.0	76.0	31.6			
D	72.2	89.7	96.0	40.0			
SYSTEM	70.8	74.1	79.3	33.0	72 <b>0</b>	321	38.8
	8 C D	C 70.8 D 72.2	B .0 .0 C 70.8 71.0 D 72.2 89.7	B .0 .0 .0 C 70.8 71.0 76.0 D 72.2 89.7 96.0	B .0 .0 .0 .0 .0 .0 .0 .0 .0 .0 .0 .0 .0	B .0 .0 .0 .0 .0 .0 .0 .0 .0 .0 .0 .0 .0	B .0 .0 .0 .0 .0 .0 .0 .0 .0 .0 .0 .0 .0

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS RETURNED TO SERVICE ON NOVEMBER 10 AFTER A FIVE WEEK SCHEDULED MAINTENANCE OUTAGE.

MODULE B WAS TAKEN OFF LINE DURING NOVEMBER DUE TO BOOSTER FAN PROBLEMS.

12/80	A	43.0	57.5	58.7	42.6				
	В	. 0	. 0		.0				
	С	53.8	69.3	70.7	51.3				
	D	60.5	78.4	80.0	58.1				
	SYSTEM	52.4	68.4	69.8	50.7	744	551	377	54.6

# ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE B REMAINED OFF LINE DURING DECEMBER DUE TO BOOSTER FAN BLADE PITCH PROBLEMS.

1/81	A	67.2	66.0	66.2	65.9				
	В	.0	.0	. 0	.0				
	С	79.8	78.2	78.4	77.9				
	D	89.2	88.9	89.2	88.7				
	SYSTEM	78.7	77.7	77.9	77.5	744	742	414	85.5

COLORADO UTE ELECTRIC: CRAIG 2 (CONT.)

RIOD	MODULE AV	/AILABILI	TY OPERABILITY		UTILIZATION	% REMOVAL SO2 PART.	PER			
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			DURING JANUAR' PITCH PROBLEMS					BOOSTER	FAN BI	LADE
2/81	A B C	32.7 65.5	64.3	32.2 64.5 .0	32.1 64.3					
	D	100.0		99.8	100.0		672	672		90.1
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			PROBLEMS WERE AND C DAMPERS	_	DURING THE	монтн штн с	PENING	THE MOI	DULE A	, В,
			DURING FEBRUAR	RY MODULE A	ALSO ENCOUNT	ERED PLUGGAG	E IN TH	iE MOIS	TURE SE	PARA-
3/81	A B C	68.5 80.6 .0		70.1 82.8 .0	67.9 80.1 .0					
	D SYSTEM	52.4 52.4	53.2	53.5 53.5	51.7 51.7		744	724	385	85.6
	** PROBLE	EMS/SOLUT	IONS/COMMENTS							
			DURING MARCH	MODULES C AN	D D EXPERIEN	CED PROBLEMS	HTIW	THE MIS	T ELIMI	INATOR
			ADDITIONAL OUD	TAGE TIME OF	MODULE C WA	S DUE TO OPE	RATIONA	AL PROB	LEMS OF	THE
/81	SYSTEM	.0	.0	.0	.0		720	<b>5</b> 96	0	59.3
	** PROBLE	EMS/SOLUT	IONS/COMMENTS							
			THE SYSTEM DIE					GED MIS	т	
/81	SYSTEM	.0	.0	.0	.0		744	744	0	
/81	SYSTEM	.0	.0	.0	.0		720	717	0	78.7
	** PROBLE	EMS/SOLUT	IONS/COMMENTS							
			DURING MAY AN					DAMAG	ED MIST	г
′/81	SYSTEM	.0	.0	.0	.0		744	686	0	61.6
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			ALL MODULES R MIST ELIMINAT		OF SERVICE D	URING JULY A	S A RES	SULT OF	THE B	ROKEN
3/81		.0	.0	.0	.0					
	B C	.0 59.7	.0 61.0	.0 61.8	.0 59.4					
	ם	39.5	40.5	41.0	39.4			_		
	SYSTEM	33. <b>1</b>	33.8	34.3	32.9		744	724	297	73.2

COLORADO UTE ELECTRIC: CRAIG 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

#### ** PROBLEMS/SOLUTIONS/COMMENTS

MODULES A AND B REMAINED DOWN DURING AUGUST AS THE UTILITY WAS WAITING FOR NEW MIST ELIMINATOR TRAYS.

MODULE D WAS UNAVAILABLE FOR PART OF THE MONTH AS A RESULT OF PROBLEMS WITH DAMPERS.

9/81	A	18.1	18.4	18.6	17.8	
	В	40.3	40.9	41.4	39.6	
	С	81.9	83.6	84.5	80.8	
	D	13.9	13.4	13.5	12.9	
	SYSTEM	51.4	52.1	52.7	50.4	

#### ** PROBLEMS/SOLUTIONS/COMMENTS

ALL FOUR MODULES BECAME OPERABLE TOWARD THE END OF THE MONTH. MODULE D HAD BEEN OUT OF SERVICE AS A RESULT OF OUTLET DAMPER PROBLEMS. MODULE A WAS PUT IN SERVICE THE THIRD WEEK OF THE MONTH AFTER HAVING THE MIST ELIMINATORS REPLACED. THE MODULES ARE NOW BEING SHUT DOWN ON A REGULAR BASIS TO CLEAN THE MIST ELIMINATORS.

720

744

744

720 315 149 32.9

696

538 81.5

739 85.7

507 82.1

10/81	A	83.9	83.7	83.8	83.7
	В	44.6	44.3	44.4	44.3
	С	85.2	84.9	85.1	84.9
	D	85.3	84.9	85.1	84.9
	SYSTEM	99.7	99.3	99.5	99.3

** PROBLEMS/SOLUTIONS/COMMENTS

DURING OCTOBER MODULE B EXPERIENCED BOOSTER FAN BEARING PROBLEMS.

PROBLEMS WITH INSTRUMENTATION HINDERED ALL FOUR MODULES DURING THE MONTH.

11/81	A	19.3	43.8	48.4	19.2
	В	1.9	4.1	4.6	1.8
	С	11.8	26.7	29.5	11.7
	D	29.6	67.3	74.4	29.4
	SYSTEM	20.8	47.3	52.3	20.7

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS SHUT DOWN FROM NOVEMBER 8 THRU NOVEMBER 23 FOR SCHEDULED MAINTENANCE.

A PROBLEM WITH MANY OF THE VALVES STICKING AT STARTUP WAS RESOLVED BY FLUSHING.

LIMESTONE BALL MILL PLUGGING PROBLEMS WERE ENCOUNTERED DURING DECEMBER.

12/81	A	33.2	33.3	33.8	32.9			
	В	32.9	33.1	33.6	32.7			
	С	88.0	88.7	89. <b>9</b>	87.6			
	D	51.6	51.9	52.6	51.3			
	SYSTEM	68.5	69.0	70.0	68.1	744	735	

^{**} PROBLEMS/SOLUTIONS/COMMENTS

DURING DECEMBER PROBLEMS WERE ENCOUNTERED WITH THE BOOSTER FAN BEARING.

MODULE D EXPERIENCED PROBLEMS WITH A BINDING OUTLET DAMPER.

					UTILIZATION	SO2 PART.	HOURS	HOURS	HOURS	FACTOR
1/82	A	81.3	83.9 77.5	84.9	81.0					
	В	75.0	77.5	78.4	74.8					
	C	77.1	79.8	80.7	77.0					
	D	83.3	86.1	87.1	83.1 100.0					
	SYSTEM	100.0	100.0	100.0	100.0		744	718	744	88.5
	** PROB	LEMS/SOLUTIO	NS/COMMENTS							
		ם	URING JANUAR	THE MIST E	LIMINATORS WE	RE CLEANED	HEEKLY.	•		
			OCKS IN THE I		S CAUSED PLUG	GING OF THE	BALL N	1ILL. 1	THE SUF	PPLIER
2/82	A	86.0	86.8	87.5	85.9					
	В	86.5	86.8 87.2 54.7 31.1 86.7	87.9	86.3					
	С	54.3	54.7	55.1	54.2					
	D	30.9	31.1	31.4	30.8					
	SYSTEM	86.0	86.7	85.9	85.9		672	665	577	85.3
	** PROB	SLEMS/SOLUTIO	NS/COMMENTS							
			URING FEBRUAR	Y MODULE D	WAS OFF-LINE	FOR 464 HOUT	RS DUE	TO A BF	SOKEN E	RECYCLE
			ROBLEMS WITH		IER UNDERFLOW	PUMP CONTRO	LLERS 1	AAS ALSO	) ENCOL	NTEREC
3/82	A	62.6	62.5	62.5	62.5					
	В	68.5	68.3	68.3	68.3					
	С	69.9	68.3 69.7	69.7	68.3 69.7					
	D		41.3							
	SYSTEM	80.9	80.6	80.6	80.6		744	744	600	80.9
	** PROB	BLEMS/SOLUTIO	NS/COMMENTS							
			OURING MARCH TOOLULE RETURN		PUMP SHAFT ON	THE D MOBU	LE WAS	REPAIRE	ED AND	THE
4/82	A	60.7	64.6	68.9	60.6					
4/82	A B	60.7 56.5	64.6 60.3	68.9 64.2	56.5					
4/82		60.7 56.5 56.0	60.3 59.6	68.9 64.2 63.5	56.5					
4/82	В	60.7 56.5 56.0 34.2	64.6 60.3 59.6 36.4	68.9 64.2 63.5 38.8	56.5 55.8					
4/82	B C	56.5 56.0 34.2	60.3 59.6	64.2 63.5 38.8	56.5 55.8		720	674	497	69.8
4/82	B C D SYSTEM	56.5 56.0 34.2	60.3 59.6 36.4 73.6	64.2 63.5 38.8	56.5 55.8 34.1		720	674	497	69.8
4/82	B C D SYSTEM	56.5 56.0 34.2 69.1 BLEMS/SOLUTIO	60.3 59.6 36.4 73.6 DNS/COMMENTS	64.2 63.5 38.8 78.5	56.5 55.8 34.1	R PROBLEMS			497	69.8
	B C D SYSTEM ** PROB	56.5 56.0 34.2 69.1 BLEMS/SOLUTIO	60.3 59.6 36.4 73.6 ONS/COMMENTS MODULE D EXPER	64.2 63.5 38.8 78.5 RIENCED SOME	56.5 55.8 34.1 69.0 E OUTLET DAMPE	:R PROBLEMS 1			497	69.8
4/82 5/82	B C D SYSTEM ** PROB	56.5 56.0 34.2 69.1 BLEMS/SOLUTION	60.3 59.6 36.4 73.6 ONS/COMMENTS MODULE D EXPER	64.2 63.5 38.8 78.5 RIENCED SOME 2.0 5.4	56.5 55.8 34.1 69.0 E OUTLET DAMPE 1.7 4.5	:R PROBLEMS 1			497	69.8
	B C D SYSTEM ** PROB	56.5 56.0 34.2 69.1 BLEMS/SOLUTION	60.3 59.6 36.4 73.6 DNS/COMMENTS MODULE D EXPER	64.2 63.5 38.8 78.5 RIENCED SOME 2.0 5.4 .0	56.5 55.8 34.1 69.0 E OUTLET DAMPE 1.7 4.5 .0	:R PROBLEMS !			497	69.8
	B C D SYSTEM ** PROB	56.5 56.0 34.2 69.1 BLEMS/SOLUTION 1.8 4.6 .0 14.1	60.3 59.6 36.4 73.6 DNS/COMMENTS MODULE D EXPER	64.2 63.5 38.8 78.5 RIENCED SOME 2.0 5.4	56.5 55.8 34.1 69.0 E OUTLET DAMPE 1.7 4.5 .0	R PROBLEMS		APRIL.		69.8
	B C D SYSTEM ** PROB	56.5 56.0 34.2 69.1 BLEMS/SOLUTION 1.8 4.6 .0 14.1	60.3 59.6 36.4 73.6 ONS/COMMENTS MODULE D EXPER 1.7 4.5 .0 14.0 6.7	64.2 63.5 38.8 78.5 RIENCED SOME 2.0 5.4 .0 16.7	56.5 55.8 34.1 69.0 E OUTLET DAMPE 1.7 4.5 .0 14.0	R PROBLEMS	DURING	APRIL.		
	B C D SYSTEM ** PROB	56.5 56.0 34.2 69.1 BLEMS/SOLUTION	60.3 59.6 36.4 73.6 ONS/COMMENTS MODULE D EXPEN 1.7 4.5 .0 14.0 6.7	64.2 63.5 38.8 78.5 RIENCED SOME 2.0 5.4 .0 16.7 8.0	56.5 55.8 34.1 69.0 E OUTLET DAMPE 1.7 4.5 .0 14.0		DURING 744	APRIL.	50	60.8
5/82	B C D SYSTEM ** PROB A B C D SYSTEM ** PROB	56.5 56.0 34.2 69.1 BLEMS/SOLUTION 1.8 4.6 .0 14.1 6.8 BLEMS/SOLUTION	60.3 59.6 36.4 73.6  DNS/COMMENTS  HODULE D EXPERIMAN 1.7 4.5 .0 14.0 6.7  DNS/COMMENTS  DURING MAY THE	64.2 63.5 38.8 78.5 RIENCED SOME 2.0 5.4 .0 16.7 8.0	56.5 55.8 34.1 69.0 E OUTLET DAMPE 1.7 4.5 .0 14.0 6.7		DURING 744	APRIL.	50	60.8
	B C D SYSTEM  ** PROB  A B C D SYSTEM  ** PROB	56.5 56.0 34.2 69.1 BLEMS/SOLUTION 1.8 4.6 .0 14.1 6.8 BLEMS/SOLUTION	60.3 59.6 36.4 73.6  DNS/COMMENTS  MODULE D EXPERIMANTS .0 14.0 6.7  DNS/COMMENTS  DURING MAY THE	64.2 63.5 38.8 78.5 RIENCED SOME 2.0 5.4 .0 16.7 8.0	56.5 55.8 34.1 69.0 E OUTLET DAMPE 1.7 4.5 .0 14.0 6.7		DURING 744	APRIL.	50	60.8
5/82	B C D SYSTEM  ** PROB  A B C D SYSTEM  ** PROB	56.5 56.0 34.2 69.1 BLEMS/SOLUTION 1.8 4.6 .0 14.1 6.8 BLEMS/SOLUTION	60.3 59.6 36.4 73.6 ONS/COMMENTS MODULE D EXPERIMENTS .0 14.0 6.7 ONS/COMMENTS OURING MAY THE	64.2 63.5 38.8 78.5 RIENCED SOME 2.0 5.4 .0 16.7 8.0 E SYSTEM WAS 51.8 .0 59.0	56.5 55.8 34.1 69.0 E OUTLET DAMPE 1.7 4.5 .0 14.0 6.7 S DOWN MOST OF 47.9 .0 54.6		DURING 744	APRIL.	50	60.8
5/82	B C D SYSTEM  ** PROB  A B C D SYSTEM  ** PROB	56.5 56.0 34.2 69.1 BLEMS/SOLUTION 1.8 4.6 .0 14.1 6.8 BLEMS/SOLUTION 48.1 .0 54.6 84.0	60.3 59.6 36.4 73.6 ONS/COMMENTS MODULE D EXPERIMENTS .0 14.0 6.7 ONS/COMMENTS OURING MAY THE	64.2 63.5 38.8 78.5 RIENCED SOME 2.0 5.4 .0 16.7 8.0 E SYSTEM WAS 51.8 .0 59.0 90.7	56.5 55.8 34.1 69.0 E OUTLET DAMPE 1.7 4.5 .0 14.0 6.7		DURING 744	APRIL. 744 THICKEN	50	60.8 AIRS.

COLORADO UTE ELECTRIC: CRAIG 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

#### ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE B WAS OFF-LINE DURING JUNE DUE TO DAMAGED TURNING VANES.

MODULES A, C, AND D WERE TAKEN DOWN FOR CLEANING AND REPAIR OF THE MIST ELIMINATOR DURING PART OF THE MONTH.

7/82	A	67.9	67.7	69.4	67.7				
	В	47.2	47.2	48.3	47.2				
	С	74.1	74.0	75.8	74.0				
	D	43.8	43.7	44.8	43.7				
	SYSTEM	77.6	77.5	79.4	77.5	744	744	577	79.6

#### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING JULY THE UNIT EXPERIENCED NUMEROUS INSTRUMENT FAILURES AS A RESULT OF EXCESSIVE MOISTURE IN THE INSTRUMENT AIR SUPPLY.

8/82	A	56.3	57.3	63.2	56.2				
	В	.0	.0	.0	.0				
	С	85.5	87.1	96.1	85.4				
	D	29.5	29.9	33.0	29.4				
	SYSTEM	57.l	58.1	64.1	57.0	744	730	424	68.8

#### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING AUGUST MODULES B AND D WERE DOWN DUE TO INOPERABLE OUTLET DAMPERS. MODULE D WAS REPAIRED BY THE END OF THE MONTH, HOWEVER REPAIRS CONTINUED ON MODULE B.

9/82	A	. 0	.0	.0	. 0				
	В	.0	. 0	.0	. 0				
	С	36.7	65.3	79.5	36.5				
	D	27.6	49.1	59.8	27.5				
	SYSTEM	21.4	38.1	46.4	21.3	72 <b>0</b>	403	153	36.9

#### ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE A WAS OUT OF SERVICE DURING SEPTEMBER DUE TO ABSORBER LINER DAMAGE.

MODULE B WAS DOWN DURING SEPTEMBER DUE TO OUTLET DAMPER PROBLEMS.

DUCTWORK PROBLEMS WERE ALSO EXPERIENCED BY MODULE B DURING THE MONTH.

THE UNIT WAS TAKEN OUT OF SERVICE ON SEPTEMBER 18 FOR AN ANNUAL OUTAGE LASTING THE REMAINDER OF THE MONTH.

10/82	A	.0	. 0	.0	.0			
	В	. 0	.0	.0	.0			
	С	50.9	57.3	94.0	50.8			
	D	25.0	28.1	46.1	24.9			
	SYSTEM	25.3	28.5	46.7	25 2	744	450	187 65 1

## ** PROBLEMS/SOLUTIONS/COMMENTS

MODULES A AND B WERE DOWN DURING OCTOBER AWAITING ABSORBER LINER REPAIRS.

MODULE D DEVELOPED A BOOSTER FAN OIL LEAK DURING THE MONTH. THE PROBLEM OCCURRED FOLLOWING THE UNIT OUTAGE AND FORCED THE MODULE OUT OF SERVICE FOR REPAIRS.

11/82 A .0 .0 .0 .0

PERIOD	MODULE		OPERABILITY			% REMOVAL SO2 PART				
	В	.0	.0	. n	. ń					
	С	63.6	63.5	63.7	63.5					
	D	93.8	93.6	94.0 52.6	93.6					
	SYSTEM	52.5	52.4	52.6	52.4		720	720	377	71.3
	** PROB	BLEMS/SOLUTIO	NS/COMMENTS							
			ODULES A AND INER REPAIRS		OUT OF SERVIC	E DURING N	OVEMBER	MAITI	NG ABS	ORBER
L2/82		.0	.0	.0	.0					
	В	. 0	.0	.0	۰.0					
	С		93.7							
	D	18.5		18.5	18.5					
	SYSTEM	37.5	37.4	37.4	37.4		744	744	278	69.6
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
			10DULES A AND LINER REPAIRS	_	OUT OF SERVIC	CE DURING D	ECEMBER	AWAITI	NG ABS	DRBER
		1	ODULE D DEVE	LOPED A BOOS	TER FAN LUBE	OIL LEAK D	URING D	ECEMBER	•	
1/83	A	.0	. 0	. 0	.0					
	В	45.8		.0 46.6	45.7					
	С		62.5	63.4	62.1					
	D	.0	. 0	.0	.0					
	SYSTEM	. 36.0	36.1	36.7	35.9		744	740	267	64.1
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
		1	ODULE A WAS I	OOWN THE ENT	IRE MONTH FOR	ABSORBER	LINER R	EPAIRS.		
			10DULE D WAS I 3 AND C ALSO					VERHAUL	. MODI	JLES
		1	10DULES B AND	C EXPERIENCE	ED DAMPER PRO	OBLEMS IN J	ANUARY.			
2/83	A	.0	.0	.0	.0					
	В		40.9	41.3						
	С	57.5	57.8	58.3	57.5					
	D	.0	.0	.0	.0					
	SYSTEM	32.7	32.9	33.2	32.7		672	668	220	67.5
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
		1	10DULES A AND	C WERE DOWN	DURING FEBRU	JARY FOR AB	SORBER	LINER R	EPAIRS	•
		•	10DULE B WAS I							
		1	10DULES B AND	D WERE DOWN	DURING FEBRU	JARY FOR BO	OSTER F.	AN REPA	IRS.	
3/83	A	34.8	36.2	37.8	34.8					
	В	49.4	51.4	53.6	49.4					
	С	.0	.0	.0	.0					
	D	.0	.0	.0	.0					
	SYSTEM	28.1	29.2	30.5	28.1		744	715	209	68.0
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
		1	ODULE C WAS !	OOWN DURING	MARCH FOR ABS	SORBER LINE	R REPAI	RS.		
4/83	A	42.2	85.0	97.4	42.2					

PERIOD		AVAILABILIT	OPERABILITY	RELIABILITY	UTILIZATION	% RE SO2	MOVAL PART.	HOURS	BOILER HOURS	HOURS	FACTOR
	B C D	.0 .0	. 0 . 0 . 0	.0	. 0 . 0 . 0						
	SYSTEM			24.3	14.0			720	357	102	34.3
	** PROE	BLEMS/SOLUTIO	NS/COMMENTS								
		C	ON APRIL 15,	THE UNIT WAS	TAKEN DOWN F	OR AN	AUNUA	L OUTAG	GE.		
		1	10DULES B AND	C WERE UNDER	RGOING LINER	REPAI	R WORK	DURIN	S THE MO	онтн.	
			10DULE D WAS I 1AHUFACTURER.	OOWN IN APRI	L AWAITING TH	E RET	URN OF	A B00	STER FAN	1 FROM	THE
<b>5</b> /83	A B	35.1 .0	48.0 .0	54.4 .0	35.1						
	С	.0	.0	.0	.0						
	D SYSTEM	.0 11.7	.0 16.0	.0 18.1	.0 11.7			744	544	87	49.5
	** PROE	BLEMS/SOLUTIO	NS/COMMENTS								
		ר	THE UNIT WAS I	DOWN MOST OF	MAY FOR AN A	NMUAL	OUTAGI	Ε.			
6/83		70.1	70.6	72.7	70.1						
	B C	9. <b>0</b> 65.8	7.9 66.3	8.2 68.3	7.9 65.8						
	D	. 0	۰.0	.0	.0						
	SYSTEM		48.3	49.7	47.9			720	715	345	69.6
	** PROE	SLEMS/SOLUTIO									
		P E	ODULE B WAS E	OOWN DURING N ONTROL.	10ST OF JUNE	DUE TO	O PROBI	LEMS WI	TH A BO	OOSTER	FAN
		ם	AMPER PROBLEM	IS ALSO ACCOU	INTED FOR THE	MODU	LE B OL	JTAGE 1	IN JUNE.		
		M M	ODULE D WAS DIANUFACTURER.	OOWN DURING .	JUNE AWAITING	THE	RETURN	OF A E	BOOSTER	FAN FR	OM THE
7/83		72.6		73.2							
	B C	92.2 49.9	37.4 52.7	37.7 53.1	37.4 52.6						
	D System	.0 71.6	.0 54.3	54.7	.0 54.2			744	742	4.07	77 7
	** PROB	BLEMS/SOLUTIO		2	34.2			777	742	403	73.7
		н	ODULE A WAS D	OWN DURING F	PART OF JULY	FOR M	IST ELI	MINATO	R CLEAN	IING.	
			ODULE C WAS E								
		H	ODULE D WAS	OUT OF SERVI	E DURING JUL	Y AWA	ITING (	DELIVER	Y OF A	вооѕте	R FAN.
8/83		75.8	75.8	75.8	75.8						
	B C	12.0 74.2	88.1 25.8	88.0 25.8	88.0 25.8						
	D	.0	.0	23.0	.0						
	SYSTEM	54.0	63.3	63.2	63.2			744	744	470	

ERIOD			OPERABILITY			% RE	MOVAL	PER			CAP.
	** PROBLE	MS/SOLUTIO	NS/COMMENTS								
		٣	ODULE D WAS D	OWN DURING	AUGUST DUE TO	BOOS	TER FAI	N REPA	IRS.		
9/83		95.3	95.6	100.0	95.3						
7/03	B	43.1	57.1	59.9							
	Č	32.8	67.4	70.7	67.2						
	D	. n	n		0						
	SYSTEM	57.1	73,4	76.9	73.2			720	718	527	75.8
	** PROBLE	MS/SOLUTIO	NS/COMMENTS								
		١	O MAJOR FGD-R	ELATED OUTA	GES WERE ENCO	UNTER	ED DUR	ING SE	TEMBER	•	
10/83	A	96.8	100.0	100.0	96.8						
	В	94.4	.8	.8	.8						
	С	.0	.0		.0						
	D	.0	.0		.0						
	SYSTEM	63.7	33.6	50.4	32.5			744	718	242	81.3
1/83	A	99.9		99.9	99.9						
	В	89.9		89.9	89.9						
	Ċ	.0		.0	.0						
	D	.0			.0						
	SYSTEM	63.3		63.3	63.3			720		456	
	** PROBLE	MS/SOLUTIO	ONS/COMMENTS				<i>و</i> .				
			NO MAJOR FGD-R 1983.	ELATED PROB	LEMS WERE ENC	OUNTE	RED DUI	RING O	TOBER	ON DNA	VEMBER
L2/83		64.0	68.5	67.1							
	В	72.2	77.3	75.7							
	C	78.2		82.0	78.2						
	D	.0	.0	75.0	0						
	SYSTEM	71.4	76.5	75.0	71.4			744	695	532	98.0
	** PROBLE	MS/SOLUTIO	ONS/COMMENTS								
		7	THE UTILITY RE	PORTED A UN	IIT TRIP ON DE	CEMBE	R 14 AI	ND 15,	1983.		
1/84	A	86.0	89.6	94.8	86.0						
	В	72.8	75.9	80.3	72.8						
	С	50.3	52.4	5 <b>5.</b> 4	50.3						
	D	.0	.0		.0						
	SYSTEM	69.7	72.6	76.8	69.7			744	714	519	
	** PROBLE	MS/SOLUTIO	ONS/COMMENTS								
			THE UTILITY REDUT OF SERVICE		THE UNIT SUF	FERED	A UNI	T-TRIP	AND SP	ENT 10	HOURS
		ו	THE UNIT LOST	HOURS ON JU	NE 27-29 DUE	TO RE	PAIRS	TO THE	THICKE	NER.	
2/84	SYSTEM							696			
	SYSTEM SYSTEM							696 744			

COLORADO UTE ELECTRIC: CRAIG 2 (CONT.)

PERFORMANCE DATA										
PERIOD MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% RE	MOVAL	PER	BOILER	FGD	CAP.
					<b>SO2</b>	PART.	HOURS	HOURS	HOURS	FACTOR

#### ** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE PERIOD OF FEBRUARY THROUGH APRIL 1984.

5/84	A	50.7	77.6	77.6	41.0
	В	51.8	98.1	98.1	51.8
	С	.0	.0		.0
	D	.0	.0	.0	.0
	SYSTEM	34.2	58.6	58.6	30.9

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE RECYCLE TANK AGITATOR WAS OUT OF SERVICE DURING MAY.

THE MIST ELIMINATOR PAD ON MODULE C WAS CLEANED DURING MAY.

6/84	A	86.2	87.0	96.3	86.2				
	В	87.1	62.3	69.0	61.7				
	С	.0	. 0		.0				
	D	75.6	74.4	82.3	73.7				
	SYSTEM	83.0	74.6	82.5	73.8		720	713	532
7/84	A	91.7	98.4	100.0	90.5				
	В	86.7	94.3	100.0	86.7				
	С	.0	.0	.0	.0				
	D	91.8	99.9	100.0	91.8	.3			
	SYSTEM	90.1	97.5	100.0	89.7		744	684	667
8/84	A	100.0	86.3	100.0	86.3				
	В	100.0	100.0	100.0	100.0				
	С	.0	.0		.0				
	D	100.0	86.0	146.1	86.0				
	SYSTEM	100.0	90.8	100.0	90.8		744	744	675

^{**} PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE REPORTED DURING THE PERIOD OF JUNE THROUGH AUGUST.

9/84 SYSTEM

720

744 393 . 230

# ** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR SEPTEMBER 1984.

# SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COMPANY NAME	COLORADO UTE E	LECTRIC
PLANT NAME	CRAIG	
UNIT NUMBER	3	
CITY	CRAIG	
STATE	COLORADO	
REGULATORY CLASSIFICATION	C	
PARTICULATE EMISSION LIMITATION - NG/J	13.	( .030 LB/MMBTU)
SO2 EMISSION LIMITATION - NG/J	86.	( .030 LB/MMBTU) ( .200 LB/MMBTU)
NOV EMISSION LIMITATION - NG/1		(****** LB/MMBTU)
NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW	900	(AAAAA ED/IIIDIO)
GROSS UNIT GENERATING CAPACITY - MW	447	
NET UNIT GENERATING CAPACITY W/FGD - MW	424	
	495	
EQUIVALENT SCRUBBED CAPACITY - MW	447	
EQUITABLE SCROODED CAPACITY - TH	447	
** UNIT DATA - BOILER AND STACK		
_	DADCOCK & UTLC	<b>0</b> V
BOILER SUPPLIER	BABCOCK & WILC	
BOILER TYPE	PULVERIZED COA	L
BOILER SERVICE LOAD  DESIGN BOILER FLUE GAS FLOW - CU.M/S  BOILER FLUE GAS TEMPEDATIBLE - C	BASE	(1570/00 4058)
DESIGN BUILDR FLUE GAS FLOW - CU.M/S	722.29	(1530600 ACFM) (**** F)
BOILER FLUE GAS TEMPERATURE - C		
STACK HEIGHT - M	183.	( 600 FT)
STACK SHELL	CONCRETE	
STACK TOP DIAMETER - M	*****	(**** FT)
WW FUEL DATA		
** FUEL DATA	COAL	
FUEL TYPE	COAL	
FUEL GRADE	SUBBITUMINOUS	( 10000 PTH (ID)
AVERAGE HEAT CONTENT - J/G	23260.	( 10000 BTU/LB)
RANGE HEAT CONTENT - BTU/LB		9100-10300
AVERAGE ASH CONTENT - %	8.00	
RANGE ASH CONTENT - %	10.0-12.0	
AVERAGE MOISTURE CONTENT - %	14.00	
RANGE MOISTURE CONTENT - %	10.0-12.0	
AVERAGE SULFUR CONTENT - %	.45	
RANGE SULFUR CONTENT - %	0.4-0.5	
AVERAGE CHLORIDE CONTENT - %	.10	
RANGE CHLORIDE CONTENT - %	0.05-0.10	
*** DARTICLE CONTROL		
*** PARTICLE CONTROL		
** FABRIC FILTER		
NUMBER	1	
PRESSURE DROP - KPA	1	( 6 0 TN_H2O)
TYPICAL GAS/CLOTH RATIO - M/MIN	1.2 7	( 6.0 IN-H2O) ( 2.3 FT/MIN)
FIRECAL GAS/CLUTT RATIO - TVHIN	• /	C.J FI/HIM
** PARTICLE SCRUBBER		
NUMBER	0	
GENERIC TYPE	NONE	
SPECIFIC TYPE	NUNE N/A	
TRADE NAME/COMMON NAME	N/A N/A	
SHELL GENERIC MATERIAL	N/A N/A	
SHELL SPECIFIC MATERIAL	N/A	
LINER GENERIC MATERIAL	N/A N/A	
LINER SPECIFIC MATERIAL GAS CONTACTING DEVICE TYPE	N/A N/A	
GAS CONTACTING DEVICE TYPE	IV A	
*** FGD SYSTEM		
. 20 0.0.0.		
** GENERAL DATA		
SALEABLE PRODUCT/THROWAWAY PRODUCT	THROWAWAY PROD	UCT
SO2 REMOVAL MODE	SFRAY DRYING	<del>~~</del> ,
PROCESS TYPE	LIME/SPRAY DRY	TNG
SYSTEM SUPPLIER	BABCOCK & WILC	
A-E FIRM	STANLEY CONSUL	
DEVELOPMENT LEVEL	FULL SCALE	Trail •
NEW/RETROFIT	NEW	
UNIT DESIGN PARTICLE REMOVAL EFFICIENCY -		
	% 99.00 85.00	
CHILDESTON SOF WELLOAME ELLICITIES Y	05.00	

CURRENT STATUS 1
COMMERCIAL START-UP 2/85
INITIAL START-UP 6/84
CONTRACT AWARDED 4/80

** DESIGN AND OPERATING PARAMETERS

** QUENCHER/PRESATURATOR

CONSTRUCTION MATERIAL GENERIC TYPE NR
CONSTRUCTION MATERIAL SPECIFIC TYPE NR

** ABSORBER

NUMBER
GENERIC TYPE
SPECIFIC TYPE
SPECIFIC TYPE
TRADE NAME/COMMON TYPE
SHELL GENERIC MATERIAL
SHELL SPECIFIC MATERIAL
SHELL MATERIAL TRADE NAME/COMMON TYPE
LINER GENERIC MATERIAL
LINER GENERIC MATERIAL
NR
LINER GENERIC MATERIAL
NR

LINER SPECIFIC MATERIAL
LINER MATERIAL TRADE NAME/COMMON TYPE
GAS CONTACTING DEVICE TYPE
NUMBER OF CONTACTING ZONES
INLET GAS FLOW - CU. M/S
S28.29
INLET GAS TEMPERATURE - C
83.3
(182 F)

INLET GAS TEMPERATURE - C 83.3 SD2 REMOVAL EFFICIENCY - % 90.0 PARTICLE REMOVAL EFFICENCY - % 99.8

** MIST ELIMINATOR

PRE-MIST ELIMINATOR/MIST ELIMINATOR

GENERIC TYPE

SPECIFIC TYPE

TRADE NAME/COMMON TYPE

CONSTRUCTION MATERIAL GENERIC TYPE

NR

CONSTRUCTION MATERIAL SPECIFIC TYPE

NR

** REHEATER

GENERIC TYPE NR
SPECIFIC TYPE NR
TRADE NAME/COMMON TYPE NR
CONSTRUCTION MATERIAL GENERIC TYPE NR
CONSTRUCTION MATERIAL SPECIFIC TYPE NR

** FANS

DESIGN NR
FUNCTION NR
APPLICATION INDUCED DRAFT
SERVICE DRY
CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL

** DAMPERS

FUNCTION NR
GENERIC TYPE NR
SPECIFIC TYPE NR
CONSTRUCTION MATERIAL GENERIC TYPE NR
CONSTRUCTION MATERIAL SPECIFIC TYPE NR
LINER GENERIC MATERIAL TYPE NR
LINER SPECIFIC MATERIAL TYPE NR

** DUCTWORK

SHELL GENERIC MATERIAL TYPE NR
SHELL SPECIFIC MATERIAL TYPE NR
LINER GENERIC MATERIAL TYPE NR
LINER SPECIFIC MATERIAL TYPE NR

** REAGENT PREPARATION EQUIPMENT

FUNCTION SLAKER
DEVICE NR
DEVICE TYPE NR

** TANKS SERVICE

NR ****

** PUMPS

SERVICE NUMBER

** SOLIDS CONCENTRATING/DEWATERING

DEVICE N/A

*** SLUDGE

** TREATMENT

METHOD N/A
DEVICE N/A
PROPRIETARY PROCESS N/A

** DISPOSAL

NATURE FINAL TYPE POND SITE TREATMENT NONE

** WATER BALANCE

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL SO2 PART. HOURS HOURS FACTOR

6/84 SYSTEM

720

7/84 SYSTEM

744

9/84 SYSTEM

720

NUMBER

# ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT INITIAL START UP COMMENCED IN JUNE 1984. COMMERCIAL START UP IS SCHEDULED FOR FEBRUARY 1985.

THE SPRAY DRYER SYSTEM AT CRAIG 3 IS THE SECOND BABCOCK AND WILCOX LIME/SPRAY DRYING PROCESS IN OPERATION TO DATE. THE UTILITY REPORTED THAT MODIFICATIONS ARE BEING MADE BASED ON PROBLEMS EXPERIENCED AT THE FIRST BABCOCK AND WILCOX INSTALLATION (LARAMIE RIVER 3).

# SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

_______

COLUMBUS & SOUTHERN OHIO ELEC COMPANY NAME CONESVILLE PLANT NAME UNIT NUMBER CONESVILLE CITY 43. ( .100 LB/MMBTU)
516. ( 1.200 LB/MMBTU)
301. ( .700 LB/MMBTU)
1890
405
377 STATE REGULATORY CLASSIFICATION PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW
GROSS UNIT GENERATING CAPACITY - MW
NET UNIT GENERATING CAPACITY W/FGD - MW
NET UNIT GENERATING CAPACITY WO/FGD - MW 373 380 EQUIVALENT SCRUBBED CAPACITY - MW 350 ** UNIT DATA - BOILER AND STACK COMBUSTION ENGINEERING BOILER SUPPLIER 596.95 (1265000 ACFM) 146.7 ( 296 F) 244. ( 800 FT) CONCRETE 7.9 BOILER TYPE DESIGN BOILER FLUE GAS FLOW - CU.M/S 596.95
BOILER FLUE GAS TEMPERATURE - C 146.7
STACK CUTT. STACK SHELL STACK TOP DIAMETER - M ** FUFL DATA FUEL TYPE COAL FUEL GRADE BITUMINOUS AVERAGE HEAT CONTENT - J/G 25237. ( 10850 BTU/LB) RANGE HEAT CONTENT - BTU/LB 10000-12000 AVERAGE ASH CONTENT - % 14.90 10.0-24.0 7.50 5.0-18.0 4.50 RANGE SULFUR CONTENT - %
AVERAGE CHLORIDE CONTENT - % 4.2-5.1 .01 RANGE CHLORIDE CONTENT - % 0.01-0.11 *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER 0 TYPE NONE ** ESP NUMBER 1 NUMBER OF SPARES 0 COLD SIDE SUPPLIER RESEARCH-COTTRELL INLET FLUE GAS CAPACITY - CU.M/S 657.8 (1393893 ACFM)
INLET FLUE GAS TEMPERATURE - C 146.7 ( 296 F)
PRESSURE DROP - KPA .5 ( 2. IN-H2O)
PARTICLE REMOVAL EFFICENCY - % 99.6 ** PARTICLE SCRUBBER NUMBER £ GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL N/A LINER GENERIC MATERIAL N/A LINER SPECIFIC MATERIAL N/A GAS CONTACTING DEVICE TYPE N/A

*** FGD SYSTEM

```
** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                                THROWAWAY PRODUCT
   SO2 REMOVAL MODE
                                                WET SCRUBBING
   PROCESS TYPE
                                                LIME
   PROCESS ADDITIVES
                                                MAG
   SYSTEM SUPPLIER
                                                AIR CORRECTION DIVISION, UOP
                                                BLACK & VEATCH
   A-E FIRM
   DEVELOPMENT LEVEL
                                                FULL SCALE
                                                NEW
   NEW/RETROFIT
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - %
                                                   99 65
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                   89.50
   ENERGY CONSUMPTION - %
                                                    1.7
   CURRENT STATUS
    COMMERCIAL START-UP
                                                 2/77
    INITIAL START-UP
                                                 1/77
    CONTRACT AWARDED
                                                10/74
** DESIGN AND OPERATING PARAMETERS
    OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                  280.0
** QUENCHER/PRESATURATOR
    NUMBER
                                                SPRAY CHAMBER
    TYPF
    SUPPLIER
                                                AIR CORRECTION DIVISION, UOP
    INLET GAS TEMPERATURE - C
                                                  141.1
                                                               ( 286 F)
    L/G RATIO - L/CU. M
                                                     .1
                                                                    .6 GAL/1000 ACFM)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                HIGH ALLOY
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                IRON BASE/NICKEL-CHROMIUM-COPPER-MOLYBDENUM
** ABSORBER
                                                 2
    NUMBER
    NUMBER OF SPARES
                                                 0
                                                PACKED TOWER
    GENERIC TYPE
    SPECIFIC TYPE
                                                MOBILE BED PACKING
    TRADE NAME/COMMON TYPE
                                                TURBULENT CONTACT ABSORBER
    SUPPLIER
                                                AIR CORRECTION DIVISION, UOP
                                                45.0 X 17.5 X 79.5
    DIMENSIONS - FT
    SHELL GENERIC MATERIAL
                                                CARBON STEEL
                                                AISI 1110
    SHELL SPECIFIC MATERIAL
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                                N/A
    LINER GENERIC MATERIAL
                                                ORGANIC
    LINER SPECIFIC MATERIAL
                                                SYNTHETIC RUBBER
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                                NEOPRENE LS-576
    GAS CONTACTING DEVICE TYPE
                                                GRID CAGES
    NUMBER OF CONTACTING ZONES
                                                 1
                                                 1988.
    LIQUID RECIRCULATION RATE - LITER/S
                                                                (31560 GPM)
    L/G RATIO - L/CU.M
                                                    6.6
                                                                ( 49.3 GAL/1000 ACF)
    GAS-SIDE PRESSURE DROP - KPA
                                                    2.0
                                                                ( 8.1 IN-H20)
    SUPERFICAL GAS VELOCITY - M/SEC
                                                    4.0
                                                                ( 13.1 FT/S)
                                                                ( 639568 ACFM)
    INLET GAS FLOW - CU. M/S
                                                  301.81
    INLET GAS TEMPERATURE - C
                                                   51.7
                                                                ( 125 F)
    SO2 REMOVAL EFFICIENCY - %
                                                   92.0
    PARTICLE REMOVAL EFFICENCY - %
                                                   99.6
** MIST ELIMINATOR
    PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                                PRIMARY COLLECTOR
    NUMBER PER SYSTEM
                                                 2
    NUMBER OF SPARES PER SYSTEM
                                                 0
    NUMBER PER MODULE
                                                 1
                                                IMPINGEMENT
    GENERIC TYPE
    SPECIFIC TYPE
                                                BAFFLE
    TRADE NAME/COMMON TYPE
                                                CLOSED VANE
    CONFIGURATION
                                                HORIZONTAL
    NUMBER OF STAGES
                                                    2
    NUMBER OF PASSES PER STAGE
                                                    4
    FREEBOARD DISTANCE - M
                                                    3.05
                                                                (10.0 FT)
                                                                ( 4.5 IN)
    DISTANCE BETWEEN STAGES - CM
                                                   11.43
    DISTANCE BETWEEN VANES
                            CM
                                                    5.1
                                                                ( 2.00 IN)
    VANE ANGLES - DEGREES
                                                  90
```

.5

( 1.9 TN-H20)

PRESSURE DROP - KPA

	SUPERFICAL GAS VELOCITY - M/S CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE WASH WATER SOURCE WASH FREQUENCY WASH RATE - L/S	3.0 ( 10.0 FT/S) ORGANIC FIBER-REINFORCED POLYESTER RECLAIMED CONTINUOUS 63.1 ( 1000 GAL/MIN)
**	REHEATER GENERIC TYPE SPECIFIC TYPE TRADE NAME/COMMON TYPE CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE	NONE N/A N/A NONE N/A
**	FANS NUMBER NUMBER OF SPARES DESIGN SUPPLIER FUNCTION APPLICATION SERVICE FLUE GAS FLOW RATE - CU.M/S FLUE GAS TEMPERATURE - C PRESSURE DROP - KPA CONSTRUCTION MATERIAL GENERIC TYPE	2 0 CENTRIFUGAL GREEN FAN UNIT FORCED DRAFT DRY 401.11 ( 850000 ACFM) 146.7 ( 296 F) .6 ( 2.0 IN-H20) CARBON STEEL
**	DAMPERS NUMBER FUNCTION GENERIC TYPE CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	2 SHUT-OFF GUILLOTINE HIGH ALLOY NICKEL BASE/CHROMIUM-IRON-MOLYBDENUM NONE N/A
**	DAMPERS NUMBER FUNCTION GENERIC TYPE CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	2 SHUT-OFF GUILLOTINE HIGH ALLOY NICKEL BASE/CHROMIUM-IRON-MOLYBDENUM NONE N/A
**	DAMPERS NUMBER FUNCTION GENERIC TYPE CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	2 CONTROL GUILLOTINE & LOUVER HIGH ALLOY NICKEL BASE/CHROMIUM-IRON-MOLYBDENUM NONE N/A
**	DUCTWORK LOCATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	INLET CARBON STEEL HIGH STRENGTH LOW ALLOY [HSLA] NONE N/A
**	DUCTWORK LOCATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	OUTLET TO DAMPER CARBON STEEL HIGH STRENGTH LOW ALLOY [HSLA] ORGANIC GLASS FLAKE-FILLED POLYESTER
**	DUCTWORK LOCATION SHELL GENERIC MATERIAL TYPE	OUTLET BEYOND DAMPER CARBON STEEL

SHELL SPECIFIC MATERIAL TYPE

LINER GENERIC MATERIAL TYPE

LINER SPECIFIC MATERIAL TYPE

HIGH STRENGTH LOW ALLOY [HSLA]
INORGANIC
CHEMICALLY-BONDED CONCRETE

** DUCTWORK
LOCATION

SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE

** REAGENT PREPARATION EQUIPMENT

FUNCTION
DEVICE
DEVICE TYPE
MANUFACTURER
NUMBER

** TANKS

SERVICE

ABSORBER RECYCLE
RECLAIMED WATER
REAGENT PREP PRODUCT
MIST ELIMINATOR WASH

** PUMPS

SERVICE

ABSORBER RECIRCULATION
LIME SLURRY TRANSFER
SLURRY MAKEUP
RECYCLE TANK DRAWOFF
MIST ELIMINATOR WASH
RECLAIM WATER
THICKENER UNDERFLOW

** SOLIDS CONCENTRATING/DEWATERING

DEVICE
NUMBER
NUMBER OF SPARES
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
BELT GENERIC MATERIAL TYPE
BELT SPECIFIC MATERIAL TYPE
FEED STREAM SOURCE
FEED STREAM CHARACTERISTICS
OUTLET STREAM CHARACTERISTICS
OUTLET STREAM DISPOSITION
OVERFLOW STREAM DISPOSITION

** SOLIDS CONCENTRATING/DEWATERING

DEVICE
NUMBER
NUMBER OF SPARES
DIMENSIONS - FT
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE
FEED STREAM SOURCE
FEED STREAM CHARACTERISTICS
OUTLET STREAM CHARACTERISTICS
OUTLET STREAM DISPOSITION
OVERFLOW STREAM DISPOSITION

NONE N/A

CARBON STEEL

SLAKER PASTE N/A

BYPASS

WALLACE & TIERNAN

HIGH STRENGTH LOW ALLOY [HSLA]

5

> NUMBER -----

VACUUM FILTER

3 1

CARBON STEEL
AISI 1110
ORGANIC
POLYPROPYLENE
THICKENER UNDERFLOW
30% SOLIDS
50% SOLIDS
TO IUCS PROCESS

TO RECLAIMED WATER TANK

THICKENER

0

0 145.0 DIA X 16.0 CARBON STEEL AISI 1110 ORGANIC EFOXY

ABSORBER BLEED 7-12% SOLIDS 30% SOLIDS

30% SOLIDS
TO IUCS THICKENER & THEN TO VACUUM FILTER

TO RECLAIMED WATER TANK

#### *** SLUDGE

COLUMBUS & SOUTHERN OHIO ELEC: CONESVILLE 5 (CONT.)

** TREATMENT

METHOD DEVICE

PROPRIETARY PROCESS INLET QUALITY - % FIXATION PUG MILL

CONVERSION SYSTEMS [POZ-O-TEC]

50.0

** DISPOSAL

NATURE TYPE LOCATION

SITE TRANSPORTATION METHOD

SITE TREATMENT

SITE DIMENSIONS

FINAL LANDFILL ON-SITE

PIPELINE/CONVEYED

NONE

80 ACRES/50 FT

** PROCESS CONTROL AND INSTRUMENTATION

CHEMICAL PARAMETERS
PHYSICAL VARIABLES
CONTROL LEVELS
MONITOR LOCATION
PROCESS CONTROL MANNE

MONITOR LOCATION
PROCESS CONTROL MANNER
PROCESS CHEMISTRY MODE

PH

RECYCLE TANK LEVEL

OUTLET PH 5.5-6.3; RECYCLE PH 7.0-7.5

SLURRY DISCHARGE FROM MODULE

AUTOMATIC FEEDBACK

** WATER BALANCE

WATER LOOP TYPE

MAKEUP WATER ADDITION - LITERS/S

CLOSED

31.5 ( 500 GPM)

** CHEMICALS AND CONSUMPTION

FUNCTION
NAME
PRINCIPAL CONSTITUENT
SOURCE/SUPPLIER
CONSUMPTION
UTILIZATION //
POINT OF ADDITION

** FGD SPARE CAPACITY INDICES ABSORBER %

** FGD SPARE COMPONENT INDICES

ABSORBER

ABSORBENT

LIME 90-95% CAO, 3-8% MGO

DRAVO 16 TPH 90.0 SLAKER

.0

.0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

12/76 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

A MAJOR FIRE IN MODULE A DELAYED THE UNIT START-UP. THE FIRE CAUSED \$2.1 MILLION DAMAGE. THE UTILITY'S INSURANCE COVERED THE DAMAGE AND A NEW SCRUBBER MODULE WILL BE PURCHASED FROM AND INSTALLED BY UOP.

THE UTILITY IS CURRENTLY CONDUCTING AIR AND WATER TESTS ON MODULE B.

1/77 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

INITIAL START-UP FOR DEBUGGING AND COMMISSIONING PURPOSES OCCURRED IN EARLY JANUARY. COMMERCIAL AVAILABILITY FOR SERVICE OCURRED ON JANUARY 27.

EARLY OPERATIONS WERE MARKED BY COLD WEATHER RELATED PROBLEMS SUCH AS FROZEN LINES AND GEARS, CRACKED FLANGES, A FROZEN LIME BELT CONVEYOR, AND A FROZEN PIPELINE FROM THE THICKENER TO THE IUCS FACILITY.

672

668

				PERFORMAT	NCE DATA							
PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% RE	MOVAL	PER	BOILER	FGD	CAP.	
, checo		.,									FACTOR	
2/77	В		43.0		43.0							

#### ** PROBLEMS/SOLUTIONS/COMMENTS

SYSTEM

ر.

COMMERCIAL START-UP OF MODULE B OCCURRED ON FEBRUARY 13, 1977. THE LONG-EST PERIOD OF CONTINUOUS OPERATION WAS 132 HOURS.

THE UTILITY REPORTED THAT THE ESP OPERATED SATISFACTORILY.

PRESSURE SURGES OCCURRED IN THE PRESATURATOR PIPING.

THE CONTINUOUS SO2 ANALYZERS OPERATED UNSATISFACTORILY.

MODULE B EXPERIENCED POOR VELOCITY DISTRIBUTION THROUGH THE TCA BEDS.

SCRUBBING LIQUOR WAS CARRYING OVER INTO THE MIST ELIMINATOR SECTION.

3/77	77 B SYSTEM		72.9		50.9	744	520
4/77	B SYSTEM	41.8	40.0	40.5	37.4	720	685

#### ** PROBLEMS/SOLUTIONS/COMMENTS

A STACK OUTLET TEMPERATURE OF 200 F IS BEING MAINTAINED IN ORDER TO MIN-IMIZE ACID RAINOUT AND STACK CORROSION PROBLEMS.

THE 316 SS PRESATURATOR AREA HAS EXPERIENCED CORROSION.

THE RUBBER LINER IN THE RECYCLE TANK HAS BEEN PEELING AWAY. THE PROBLEM APPEARED TO BE APPLICATION-RELATED.

SOME PLUGGING HAS OCCURRED IN THE TUBE THICKENERS.

THE QUALITY OF THE LIME SLURRY HAS BEEN A PROBLEM AREA. ROCKS UP TO FIVE INCHES IN DIAMETER HAVE BEEN DETECTED. THIS HAS PROMPTED DRAVO TO INSTALL MECHANICAL SEPARATORS AND METAL DETECTORS AT THE LIME SHIPMENT FACILITY.

5/77	B System	58.0	50.0	51.0	48.0	744	712
6/77	B SYSTEM	66.0	59.0	60.0	58.0	720	713
7/77	B SYSTEM	.0	.0	.0	.0	744	744

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE B-SIDE MODULE DID NOT OPERATE THE ENTIRE MONTH PENDING COMPLETION OF A NUMBER OF NECESSARY MODIFICATIONS AND REPAIRS.

MODIFICATIONS WERE MADE TO THE UNIT PROCESS CONTROL SYSTEM.

MODIFICATIONS WERE MADE TO THE UNIT INSTRUMENTATION SYSTEM.

REPAIRS WERE MADE TO THE ABSORBER LINER.

REPAIRS WERE MADE TO THE PIPING BETWEEN THE THICKENER AND IUCS BUILDING.

THE UTILITY IS CURRENTLY PLANNING TO CONDUCT A PARTICULATE DROP TEST

COLUMBUS & SOUTHERN OHIO ELEC: CONESVILLE 5 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

SCHEDULED FOR SEPTEMBER 1977.

THE REPLACEMENT A-SIDE TCA MODULE REPLACING THE ORIGINAL MODULE DESTROYED BY FIRE IN DECEMBER 1976 IS EXPECTED TO BE AVAILABLE FOR COMMERCIAL SERVICE IN JANUARY 1978.

8/77	B SYSTEM	.0	.0	.0	.0	744	613
9/77	B SYSTEM	52.9	39.9	46.9	26.0	720	469

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE PARTICULATE DROP TEST SCHEDULED FOR SEPTEMBER 1977 WAS PUSHED BACK TO THE WEEK OF OCTOBER 24 1977.

THE SCRUBBER WAS NOT OPERATED THE ENTIRE MONTH OF AUGUST. REPAIRS AND MODIFICATIONS CONTINUED UNTIL SEPTEMBER 13. THERE WERE SOME WEATHER-RELATED DELAYS.

10/77	B SYSTEM	32.0	24.0	25.0	18.0	744	559	
11/77	A	10.0	4.0	4.0	4.0			
	В	33.0	33.0	33.0	33.0			
	SYSTEM	21.5	18.5	18.5	18.5	720	715	133

#### ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE A WENT ON LINE NOVEMBER 21. DURING LOW LOAD PERIODS SOLIDS BUILD UP TENDED TO CAUSE PLUGGING BECAUSE OF LOW FLOW RATES. DURING THE LOW LOAD PERIODS ALL GAS WAS DUCTED THROUGH ONE MODULE WHILE THE OTHER WAS SHUT DOWN.

THE SCRUBBER WAS DOWN FROM OCTOBER 10 TO NOVEMBER 10 FOR RELINING WITH NEOPRENE RUBBER.

12/77	A	93.0	64.0	62.0	22.0			
	В	97.0	79.0	76.0	27.0			
	SYSTEM	95.0	71.5	69.0	24.5	744	252	180

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WENT DOWN DECEMBER 12 FOR A 3-MONTH SCHEDULED OUTAGE. MODULE A BEGAN COMMERCIAL OPERATIONS DECEMBER 3 OPERATING AS MUCH AS POSSIBLE THROUGH DECEMBER 12. MODULE B OPERATED DECEMBER 1 THROUGH 12. DURING THE SHUTDOWN THE UTILITY WILL DECIDE IF THE SYSTEM SUPPLIERS HAVE MET SPECS ON THE BOILER AND TURBINES. THE UNIT IS SCHEDULED TO BE BACK ON LINE IN MID-MARCH BUT THIS MAY BE PUSHED BACK TO APRIL 1.

DURING THE DECEMBER TO MARCH 1978 SHUTDOWN THE CARBON STEEL FLUE WILL BE REPLACED WITH AN ACID-BRICK LINING.

1/78	SYSTEM	.0			. 0	744	0	0	.0
2/78	SYSTEM	.0			.0	672	0	0	.0
3/78	A B System	20.0 20.0 20.0	19.0 15.8 17.4	64.0 54.0 59.0	10.0 8.0 9.0	744	379	66	

PERFORMANCE DATA									
PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION	% REN	10VAL	PER	BOILER	FGD	CAP.			
• • • • • • • • • • • • • • • • • • • •						FACTOR			

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT STARTED UP AGAIN ON MARCH 16.

PH CONTROLS AND SO2 ANALYZERS HAVE EXPERIENCED OPERATIONAL PROBLEMS.

IMPURITIES IN THE LIME HAVE CAUSED PLUGGING PROBLEMS.

4/78	A	67.0	58.0	61.0	58.0			
	В	65.0	59.0	63.0	59.0			
	SYSTEM	66.0	58.5	62.0	58.5	720	716	421

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE SYSTEM WAS DOWN DUE TO AN EXCESS OF FLOCCULANT IN THE THICKENER.

EXCESS FLOCCULANT IN THE THICKENER YIELDED A HIGH SOLIDS LEVEL IN THE OVERFLOW AND RESULTED IN PLUGGING PROBLEMS IN THE ABSORBER MODULES.

5/78	A	52.0	45.0	45.0	44.0			
	В	54.0	50.0	51.0	69.0			
	SYSTEM	53.0	47.5	48.0	56.5	744	720	420

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE SYSTEM WAS TAKEN OUT OF SERVICE BECAUSE OF CONTINUED PROBLEMS WITH THE FLOCCULANT FEED SYSTEM. THE THICKENER WAS EMPTIED TO RESTORE PROPER FLOCCULANT BALANCE.

6/78	A	48.0	37.0	37.0	37.0			
	В	30.0	30.0	30.0	30.0			
	SYSTEM	39 <b>.0</b>	33.5	33.5	33.5	720	720	243

#### ** PROBLEMS/SOLUTIONS/COMMENTS

AN FRP PIPING FAILURE IN THE MIST ELIMINATOR WASH SYSTEM OCCURRED.

7/78	A	66.0	66.0	66.0	64.0			
	В	43.0	33.0	33.0	32.0			
	SYSTEM	54.5	49.5	49.5	49.0	744	727	359

#### ** PROBLEMS/SOLUTIONS/COMMENTS

OUTAGE TIME WAS DUE TO PLUGGING IN THE MIST ELIMINATOR AND SCRUBBER BALL REGIONS.

8/78	A	18.0	20.0	20.0	18.0			
	В	18.0	21.0	21.0	18.0			
	SYSTEM	18.0	20.5	20.5	18.0	744	667	135

# ** PROBLEMS/SOLUTIONS/COMMENTS

THE FORCED OUTAGE TIME WAS DUE, IN PART, TO TIME REQUIRED TO REMOVE SCALE FROM THE MIST ELIMINATOR.

THE FORCED OUTAGE TIME WAS DUE, IN PART, TO TIME REQUIRED TO REPLACE SOME OF THE PING PONG BALLS IN THE MODULES.

THE UTILITY EXPERIENCED BYPASS DAMPER PROBLEMS DURING THE PERIOD.

PROBLEMS OCCURRED RELATED TO BROKEN SLUDGE LINES AND PLUGGING IN THE LIME SLURRY FEED LINES.

					NCE DATA						
PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% REI	MOVAL PART.	PER HOURS	BOILER HOURS	FGD HOURS	CAP. FACTOR
9/78	A	61.0	46.0	55.0	45.0						
	В	54.0	44.0	53.0	43.0						
	SYSTEM	54.0 57.5	45.0	54.0	44.0			720	707	316	
10/78	A	72.0	37.0	38.0	36.0						
	В	82.0	46.0	47.0	45.0						
	SYSTEM	77.0	41.5	42.5	45.0 40.5			744	713	301	
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
		}	DAMPER DRIVE	PROBLEMS WE	RE REPORTED B	Y THE	UTILI	ry.			
					LURE WAS OBSE				ONE OF	THE	
11/78	A B	43.0	29.0 74.0	29.0	25.0						
	В	84.0	74.0	75.0	66.0						
	SYSTEM	63.5	51.5	52.0	45.5			720	642	331	
12/78	A	6.6 33.1	۰.3	.3	.3						
	В	33.1	36.3	.3 36.6	.3 30.0						
	SYSTEM	19.8	18.3	18.4	15.1			744	609	112	
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			THE LOW HOURS	S FOR THIS P	ERIOD ARE ATT	RIBUTE	D TO F	REEZE	UPS.		
1/79	SYSTEM	.0	.0	.0	.0			744	602	0	
2/79	SYSTEM	.0	.0	.0	.0			672	629	0	
	** PROB	BLEMS/SOLUTION	NS/COMMENTS								
			HE SYSTEM WAS INTER WEATHER		E DURING JANU.	ARY A	D FEBR	RUARY E	BECAUSE	OF SEV	ERE
3/79		50.0	49.0	50.0	43.0						
	В	.0	.0	.0	.0						
	SYSTEM	.0 25.0	24.5	25.0	21.5			744	652	160	
4/79	A	17.0	58.0	73.0	12.0						
	В	. 0	. 0	.0	.0						
	SYSTEM	8.5	29.0	36.5	6.0			720	149	43	
	** PROB	BLEMS/SOLUTIO	NS/COMMENTS								
		M(S)	DOULE B DID N	NOT OPERATE RESATURATOR	DURING MARCH A INLET DUCT WH:	AND AF	RIL BE	CAUSE REPAI	OF SEVE	RE COR	RO-
5/79	SYSTEM	.0	.0	.0	.0			744	744	0	
	** PROE	BLEMS/SOLUTION	NS/COMMENTS								
		RI	EPAIRS WERE 1	ADE TO THE	SEAL BETWEEN	THE TH	ICKENE	R BASE	E AND SI	[DEWALI	
		Ti	HE FGD SYSTEM	1 WAS DOWN D	URING MAY FOR	AN AA	MUAL (	UTAGE.	,		
6/79	A	69.0	35.0	36.0	77. ^						
	В	50.0	21.0	22.0	33.0 20.0						
	SYSTEM	59.5	28.0	29.0	26.5			720	470	101	
			23.0	L 7. U	20.5			720	67 <b>0</b>	191	

# PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS FACTOR

#### ** PROBLEMS/SOLUTIONS/COMMENTS

PLUGGED PH LINES WERE A PROBLEM DURING MAY AND JUNE.

FLYASH CONVEYING PROBLEMS RESULTED IN ABOUT A TWO DAY OUTAGE.

OUTLET DAMPER PROBLEMS WERE REPORTED BY THE UTILITY.

7/79	A	75.3	76.3	77.6	69.0				
	В	93.4	89.8	90.8	80.6				
	SYSTEM	84.4	82.8	84.2	74.8	744	672	557	
8/79	A	86.6	24.7	25.0	10.1				
	В	85.6	22.7	23.0	9.3				
	SYSTEM	86.1	23.7	24.0	9.7	744	305	72	
9/79	A	89.3	52.6	59. <b>5</b>	27.9				
	В	95.9	51.3	58.0	27.2				
	SYSTEM	92.6	51.9	58.8	27.6	720	383	199	
10/79	A	53.2	76.3	77.0	45.4				
	В	47.8	77.4	78.1	46.1				
	SYSTEM	50.5	76.9	77.6	45.8	744	443	341	
11/79	A	74.0	90.0	91.0	52.0				
	В	70.0	88.0	89.0	51.0				
	SYSTEM	72.0	89.0	90.0	51.2	720	414	369	
12/79	SYSTEM	.0			.0	744	0	0	.0

## ** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE LAST HALF OF 1979 THE UNIT EXPERIENCED PROBLEMS WITH THE LIME BLOWER COMPRESSOR MOTOR.

CAVITATION WAS SITED IN THE SLUDGE PUMP.

THE FLYASH CONVEYOR SYSTEM CAUSED PROBLEMS DURING THE LATTER HALF OF THE YEAR.

PLUGGING IN THE REAGENT CIRCULATION SYSTEMS WAS ENCOUNTERED.

THERE WERE PROBLEMS WITH THE GUIDE BARS AND SEALS IN THE INLET DAMPER DURING THE LAST HALF OF 1979.

				•				
1/80 A	89.0	38.0	45.0	13.0				
В	93.0	50.0	59.0	17.0				
SYSTEM	91.0	44.0	52.0	15.0	744	257	113	21.4

#### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING JANUARY A BOILER OUTAGE OCCURRED FROM THE FIRST OF THE MONTH TO JANUARY 20, DURING WHICH TIME MAINTENANCE WAS PERFORMED ON THE FGD SYSTEM.

2/80	A	90.0	63.0	77.0	31.0				
	В	93.0	69.0	84.0	34.0				
	SYSTEM	92.0	66.0	81.0	33.0	696	343	226	31.4

#### ** PROBLEMS/SOLUTIONS/COMMENTS

A BOILER OUTAGE LASTING APPROXIMATELY 17 DAYS ALSO OCCURRED DURING FEBRUARY.

PERIOD	MODULE AVAI	LABILI	TY OPERABILITY	RELIABILITY	UTILIZATION	% REMOVA SO2 PAR	L PER T. HOURS	BOILER HOURS	FGD HOURS	CAP. FACTOR
************	<u></u>		IN FEBRUARY, M SYSTEM OUTAGE	IST ELIMINAT						
3/80	A B SYSTEM	88.0 88.0 88.0	82.0 81.0 82.0	82.0 82.0 82.0	82.0 81.0 82.0		744	744	606	75.4
	** PROBLEMS	/SOLUT	IONS/COMMENTS							
			DURING MARCH F PROCESS AND SO REQUIRED REPLA	ME OUTAGE TI	ME RESULTED	. ALSO DU	RING MARC	H SOME		
			THE MAJORITY OF PROBLEMS WITH				E WAS DUE	TO CO	NIUNIT	G
4/80	A B System	94.6 74.9 84.7	84.4 65.8 75.2	87.7 68.4 78.0	78.9 61.5 70.3		720	673	506	63.1
			IONS/COMMENTS							
			CONTINUAL PROE THE CAUSES OF				OR HOSES,	N CHA	ÖZZLES	WERE
5/80			86.2 84.3							
	SYSTEM	91.3	85.2	85.2	85.2		744	744	634	69.5
	** PROBLEMS	S/SOLUT	IONS/COMMENTS							
			IN MAY, CONTRO OUTAGE TIME.	LS AND INSTR	UMENTATION	DEVELOPED	PROBLEMS	THAT C	AUSED S	OME
6/80	<b>A</b> B	89.6 94.3	71.0 74.8	71.0	70.7					
	SYSTEM	91.9	72.9	74.8 72.9	72.6		720	717	523	65.1
	** PROBLEMS	/SOLUT	IONS/COMMENTS							
			EXTERNAL CAUSE PROBLEMS, ETC.	S (IUCS DISP ) WERE RESPO	OSAL FACILI NSIBLE FOR	TY, LOW UN THE MAJORI	IT DEMAND TY OF THE	), SERV	ICE WAT	ER
7/80		90.6		72.4						
	SYSTEM	88.8 89.7	82. <b>0</b> 76.4	84. <b>0</b> 78.2	50.8 47.3		744	461	352	36.6
	** PROBLEMS	S/SOLUT	IONS/COMMENTS							
			THE PRESATURAT		NOZZLES PL	UGGED CAUS	ING THE L	OT TIM	SHUT D	סאא
8/80	A	98.0	83.5	84.9	48.5					
	B SYSTEM	95.4 96.7	88.8 86.2	90.4 87.6	51.6 50.1		744	432	373	40.0
	** PROBLEMS	S/SOLUT	IONS/COMMENTS							
			THE UTILITY RE			TH THE REC	LAIM WATE	R SYST	EM OCCL	JRRED
9/80	A	87.6	73.4	74.4	73.1					
	B System	88.8 88.2	85.1 79.2	86.3 80.3	82.0 78.9		720	717	<b>E</b>	71 E
			17.6	00.3	10.7		720	/1/	200	71.5

	MODULE AVAILA		TY OPERABILITY				PER	BOILER	FGD	CAP. FACTOR
	** PROBLEMS/S	SOLUT:	IONS/COMMENTS							
			DURING THE JUL PROBLEM.	Y-SEPTEMBER	PERIOD INLET	DAMPER SEA	L LEAKI	ING WAS	A MAJO	IR
			THE PRESATURAT		CONTINUED IN	SEPTEMBER	CAUSING	ADDIT:	IONAL C	UTAGE
10/80	В 8	92.7 89.2 91.0	80.0	80.8 82.9 81.9			744	727	571	E0 7
			IONS/COMMENTS	01.7	70.7		/	,23	3/1	37.7
	, No Desirior		DURING OCTOBER PROBLEMS.	R MINOR OUTA	GES WERE THE	RESULT OF D	AMPER A	ND AGI.	TATOR M	IOTOR
11/80	A :	79.0	35.7	36.9	31.3					
		86.1 82.6		66.8 <b>51.</b> 9	56.5		720	430	316	75 0
			IONS/COMMENTS	31.7	43.7		720	630	310	33.7
			THE LOW SYSTEM SULT OF A 28 H AGITATOR MOTOR	HOUR OUTAGE				-		RE-
			ADDITIONAL MIN TEMPERATURE PE NOVEMBER.							s,
12/80			88.8	89.2	82.2					
		90.9 92.0	86.6 87.7	85.3 87.2	80.2 81.2		744	689	604	72.6
	** PROBLEMS/	SOLUT	IONS/COMMENTS							
	** PROBLEMS/	SOLUT	IONS/COMMENTS  DURING DECEMBINERE ENCOUNTER		TY REPORTED T	OLAM ON TAH	R FGD-R	RELATED	PROBLE	:MS
1/81			DURING DECEMBE			OLAM ON TAH	R FGD-R	RELATED	PROBLE	:MS
1/81	A B	90.6 90.5	DURING DECEMBI WERE ENCOUNTER 85.7 86.0	87.4 84.9	77.4 77.2	HAT NO MAJO				
1/81	A B SYSTEM	90.6 90.5 90.5	DURING DECEMBE WERE ENCOUNTER 85.7 86.0 86.0	87.4	77.4	OLAM ON TAH	R FGD-F 744			:MS 71.0
1/81	A B SYSTEM	90.6 90.5 90.5	DURING DECEMBI WERE ENCOUNTER 85.7 86.0	87.4 84.9 84.9 84.9	77.4 77.2 77.2		744	672	575	71.0
1/81	A B SYSTEM SYSTEM ** PROBLEMS/S	90.6 90.5 90.5	DURING DECEMBE WERE ENCOUNTER 85.7 86.0 86.0 10NS/COMMENTS	87.4 84.9 84.9 84.9	77.4 77.2 77.2		744	672	575	71.0
	A B SYSTEM ** PROBLEMS/S	90.6 90.5 90.5 SOLUT 93.2 95.4	DURING DECEMBE WERE ENCOUNTER  85.7 86.0 86.0 IONS/COMMENTS  DURING JANUAR WERE ENCOUNTER  89.9 94.9	87.4 84.9 84.9 Y THE UTILIT RED. 91.2 93.6	77.4 77.2 77.2 Y REPORTED TH 83.4 88.1		744 FGD-RE	672 ELATED	575 PROBLEM	71.0 1S
	A B SYSTEM ** PROBLEMS/S A B SYSTEM	90.6 90.5 90.5 SOLUT 93.2 95.4 94.2	DURING DECEMBE WERE ENCOUNTER 85.7 86.0 86.0 IONS/COMMENTS DURING JANUAR WERE ENCOUNTER 89.9 94.9 92.3	87.4 84.9 84.9 84.9 Y THE UTILIT RED. 91.2	77.4 77.2 77.2 Y REPORTED TH 83.4		744	672 ELATED	575 PROBLEM	71.0
	A B SYSTEM ** PROBLEMS/S A B SYSTEM	90.6 90.5 90.5 SOLUT 93.2 95.4 94.2	DURING DECEMBE WERE ENCOUNTER  85.7 86.0 86.0 IONS/COMMENTS  DURING JANUAR WERE ENCOUNTER  89.9 94.9	87.4 84.9 84.9 Y THE UTILIT RED. 91.2 93.6 92.4	77.4 77.2 77.2 Y REPORTED TH 83.4 88.1 85.7	AT NO MAJOR	744 FGD-RE 672	672 ELATED 624	575 PROBLEM 576	71.0 1S
	A B SYSTEM  ** PROBLEMS/S  A B SYSTEM  ** PROBLEMS/S	90.6 90.5 90.5 SOLUT 93.2 95.4 94.2	DURING DECEMBE WERE ENCOUNTER  85.7 86.0 86.0  IONS/COMMENTS  DURING JANUAR WERE ENCOUNTER  89.9 94.9 92.3  IONS/COMMENTS  DURING FEBRUAR	87.4 84.9 84.9 Y THE UTILIT RED. 91.2 93.6 92.4	77.4 77.2 77.2 Y REPORTED TH 83.4 88.1 85.7	AT NO MAJOR	744 FGD-RE 672	672 ELATED 624	575 PROBLEM 576	71.0 1S

COLUMBUS & SOUTHERN OHIO ELEC: CONESVILLE 5 (CONT.)

PERIOD	MODULE	AVAÎLABÎLÎT	Y OPERABILITY	RELIABILITY	UTILIZATION	N % REI	MOVAL	PER	BOILER HOURS	FGD HOURS	CAP. FACTOR
			ONE COMMENTS			_					
	** PRO	315W2\201011	ONS/COMMENTS					35 055	I THE E	on ecur	
			DURING MOST OF MAINTENANCE.	MARCH THE	BOILER AND I	F6D 515	IEM MEI	KE UFF	EINE FI	JK SCH	נטטננט
4/81		98.9		90.1							
	B SYSTEM	94.3 96.6		84.5 87.3	60.6 63.8			720	555	450	
5/81	A	99.7	100.0	100.0	95.0						
	В		100.0	100.0	95.0			744	707	707	
	SYSTEM	99.7	100.0	100.0	95.0			/44	707	707	
6/81	A		100.0	100.0	96.4						
	B	98.5 99.0	100.0 100.0	100.0 100.0				720	698	698	
				100.0	, , ,				2.0		
	** PRO	BLEMS/SOLUT	CONS/COMMENTS								
			THE UTILITY REDURING THE SEC			PERATIO	NAL PR	OBLEMS	WERE E	NCOUNT	ERED
7/81	A	99.8	100.0	100.0	55.4						
	В	100.0	100.0	100.0	55.4			7.,	430	410	
	SYSTEM	99.9	100.0	100.0	55.4			744	412	412	
	** PRO	BLEMS/SOLUT	IONS/COMMENTS								
			DURING JULY, T BOILER FEED PU		ONLY OPERATE	D 412 H	OURS A	S A RE	SULT OF	FAILU	RE OF A
8/81	A B	99.0		95.0	43.0						
		99.0			39.0			744	400	705	
	SYSTEM	99.0		91.5				744	422	305	
9/81		100.0	59.0	100.0	6.0						
	B SYSTEM	87.0 93.5	40.0	81.0 90.5	5.0			720	69	41	
	** PRO	BLEMS/SOLUT	IONS/COMMENTS								
			SEVERE OUTLET FAILED DUE TO IS LOOKING INT	INADEQUATE	STRENGTH OF	THE SU	PPORTI	NG MES			
			UNIT 5 WAS REN THE UNIT IS NO THIS OUTAGE PE	T EXPECTED	TO BE BROUG	HT BACK	ON LI	NE UNT	IL DECE	MBER.	EMAND.
10/81	A	100.0	.0	.0	.0						
	B	100.0	.0	.0	.0			7//		•	
	SYSTEM	100.0	.0	.0	.0			744		0	
	** PRO	BLEMS/SOLUT	IONS/COMMENTS								
			DURING OCTOBER DUCTWORK. THE ING THE GUNITE	IS INCLUDED							
11/81	A	27.0	.0	.0	.0						
	В	27.0	. 0	.0	.0						
	SYSTEM	27.0	.0	. 0	.0			720		C	)

	 	PERFORMAN	CE DATA	 	 	 
PERIOD MODULE		_				
PERIOD HODGEL	 OI ENABLEET !	Keelnbeeli	0.22227.207.			FACTOR

#### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING NOVEMBER MAJOR MODIFICATION TO THE FGD SYSTEM DUCTWORK WAS PERFORMED. THIS WORK INCLUDED REPAIRING THE CORRODED SUPPORTS AND RECOATING WITH GUNITE.

ADDITIONAL OUTAGE TIME DURING THE MONTH WAS DUE TO GENERAL FGD MAINTENANCE.

12/81	A	84.0	82.0	86.0	77.0			
	В	84.0	82.0	86.0	77.0			
	SYSTEM	84.0	82.0	86.0	77.0	744	699	573

#### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING DECEMBER TEST WERE CONDUCTED ON THE ESP.

ADDITIONAL OUTAGE TIME DURING THE MONTH WAS DUE TO HIGH THICKENER SOLIDS AND PROBLEMS WITH THE FLYASH HANDLING SYSTEM.

1/82	A	97.0	83.0	87.0	69.0			
	В	88.0	81.0	85.0	67.0			
	SYSTEM	92.5	82.0	86.0	68.0	744	617	506
2/82	A	99.0	80.0	89.0	64.0			
	В	98.0	76.0	84. <b>0</b>	60.0			
	SYSTEM	98.5	78. <b>0</b>	86.5	62.0	672	535	417
3/82	A	100.0	89.0	95.0	76.0			
	В	93.0	90.0	96.0	77.0			
	SYSTEM	96.5	89.5	95.5	76.5	744	636	569

# ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE FIRST QUARTER OF 1982.

4/82	A	98.0	81.0	89.0	50.0			
	В	67.0	62.0	67.0	38.0			
	SYSTEM	82.5	71.5	78.0	44.0	720	443	317
5/82	A	100.0	83.0	98. <b>0</b>	48.0			
	В	100.0	78.0	92. <b>0</b>	46.0			
	SYSTEM	100.0	80.5	95.0	47.0	744	434	350
6/82	A	100.0	77.0	93.0	17.0			
	В	98.0	64.0	77.0	14.0			
	SYSTEM	99.0	70.5	85.0	15.5	720	158	112

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE SECOND QUARTER 1982.

7/82	5A 5B System	94.6 94.3 94.4	93.7 85.6 89.6	96.5 88.2 92.3	58.1 53.1 55.6	744	461	414	43.9
8/82	5A 5B System	99.2 99.5 99.4	89.4 99.1 94.2	87.5 97.0 92.3	66.9 74.1 70.5	744	557	524	56.2
9/82	5A	96.4	89.7	92.3	55.5				

COLUMBUS & SOUTHERN OHIO ELEC: CONESVILLE 5 (CONT.)

PERIOD	MODULE AV		Y OPERABILITY			502			BOILER HOURS		
	5B		83.5								
	SYSTEM		86.6	89.1	53.5			720	445	386	47.5
10/82	5A	86.4	88.0	89.1	64.2						
	5B	86.3	86.5	87.6	63.1						_
	SYSTEM	86.3	87.3	88.4	63.7			744	<b>5</b> 43	474	55.1
	** PROBLE	MS/SOLUT	ONS/COMMENTS								
			THE UTILITY REDURING THE PER					OBLEMS	WERE E	NCOUNTE	ERED
11/82	5A	.0			.0						
	58	.0			.0						
	SYSTEM	.0			.0			720	0		.0
	** PROBLE	EMS/SOLUT	ONS/COMMENTS								
			UNIT 5 WAS OUT	OF SERVICE	DURING NOVEM	BER F	OR AN	ANNUAL	OUTAGE	•	
12/82	5A	23.7			.0						
	5B	23.7			.0			_			
	SYSTEM	23.7			.0			744	0		.0
	** PROBLE	MS/SOLUT	ONS/COMMENTS								
			THE ANNUAL OUT.	AGE CONTINUE	D FOR UNIT 5	THRO	UGHOUT	THE M	ONTH OF	DECEME	BER.
1/83			58.7	62.9	19.5						
	5B SYSTEM	92.4	70.7 64.7	75.8	23.5				249	140	24.0
	3131511	90.5	0.4.7	69.4	61.3			/44			
				69.4	21.5			744	240	160	
			ONS/COMMENTS UNIT 5 WAS PLAN			NG JA	MUARY I				
	** PROBLE	EMS/SOLUT	ONS/COMMENTS UNIT 5 WAS PLAY			NG JA	NUARY				
2/83	** PROBLE	EMS/SOLUT	ONS/COMMENTS UNIT 5 WAS PLAY	CED BACK IN	SERVICE DURI	ING JAI	NUARY I				
2/83	** PROBLE	91.8 88.3	ONS/COMMENTS UNIT 5 WAS PLAY OUTAGE.  89.3 86.6	CED BACK IN 89.7 87.0	SERVICE DURI 87.2 84.5	ING JA	MUARY I	FOLLOW	ING THE	ANNUAL	L
2/83	** PROBLE	91.8 88.3	ONS/COMMENTS UNIT 5 WAS PLAY OUTAGE.  89.3	CED BACK IN 89.7 87.0	SERVICE DURI 87.2 84.5	HG JA	MUARY I	FOLLOW		ANNUAL	
2/83	** PROBLE  5A 58 SYSTEM	91.8 88.3 90.0	ONS/COMMENTS UNIT 5 WAS PLAY OUTAGE.  89.3 86.6	CED BACK IN 89.7 87.0	SERVICE DURI 87.2 84.5	NG JA	NUARY I	FOLLOW	ING THE	ANNUAL	L
2/83	** PROBLE  5A 58 SYSTEM	91.8 88.3 90.0	ONS/COMMENTS UNIT 5 WAS PLAY OUTAGE.  89.3 86.6 88.0	SED BACK IN  89.7  87.0  88.3  ARY 16, 1983  TO INCLUDE OUTAGE. THE	SERVICE DURI  87.2  84.5  85.8  3, THE UTILIT PERIODS WHEN	Y WAS I SCRU I CONF	CONSI BBER M ORMS T	FOLLOW: 672 DERING AINTEN. 0 THE (	ING THE  656  FGD SY: ANCE WA: CORRECT	ANNUAL 577 STEM S PERFO DEFIN:	60.7
2/83	** PROBLE  5A 58 SYSTEM  ** PROBLE	91.8 88.3 90.0	CONS/COMMENTS  UNIT 5 WAS PLAY OUTAGE.  89.3 86.6 88.0  CONS/COMMENTS  PRIOR TO FEBRU AVAILABLE TIME DURING A UNIT OF AVAILABILIT PERIODS.	89.7 87.0 88.3 ARY 16, 1983 TO INCLUDE DUTAGE. THE	SERVICE DURI  87.2  84.5  85.8  5, THE UTILIT PERIODS WHEN UTILITY NOW ERS THE SCRU	Y WAS I SCRU I CONF	CONSI BBER M ORMS T	FOLLOW: 672 DERING AINTEN. 0 THE (	ING THE  656  FGD SY: ANCE WA: CORRECT	ANNUAL 577 STEM S PERFO DEFIN:	60.7
	** PROBLE  5A 58 SYSTEM  ** PROBLE	91.8 88.3 90.0 EMS/SOLUT:	ONS/COMMENTS  UNIT 5 WAS PLAY OUTAGE.  89.3 86.6 88.0  CONS/COMMENTS  PRIOR TO FEBRU AVAILABLE TIME DURING A UNIT OF AVAILABILIT	SED BACK IN  89.7  87.0  88.3  ARY 16, 1983  TO INCLUDE OUTAGE. THE	SERVICE DURI  87.2  84.5  85.8  3, THE UTILIT PERIODS WHEN	Y WAS I SCRU I CONF	CONSI BBER M ORMS T	FOLLOW: 672 DERING AINTEN. 0 THE (	ING THE  656  FGD SY: ANCE WA: CORRECT	ANNUAL 577 STEM S PERFO DEFIN:	60.7
	** PROBLE  5A 58 SYSTEM  ** PROBLE	91.8 88.3 90.0 EMS/SOLUTE	CONS/COMMENTS  UNIT 5 WAS PLAY OUTAGE.  89.3 86.6 88.0  CONS/COMMENTS  PRIOR TO FEBRU AVAILABLE TIME DURING A UNIT OF AVAILABILIT PERIODS.  93.5	89.7 87.0 88.3 ARY 16, 1983 TO INCLUDE OUTAGE. THE Y AND CONSID	SERVICE DURI  87.2  84.5  85.8  3, THE UTILIT PERIODS WHEN EUTILITY NOW ERS THE SCRU	Y WAS I SCRU I CONF	CONSI BBER M ORMS T	FOLLOW: 672 DERING AINTEN. 0 THE (	FGD SYS	577 STEM S PERFO DEFINITHESE	60.7 DRMED ITION
	** PROBLE  5A 5B SYSTEM  ** PROBLE  5A 5B SYSTEM	91.8 88.3 90.0 EMS/SOLUT: 92.3 90.5 91.4	ONS/COMMENTS  UNIT 5 WAS PLAY OUTAGE.  89.3 86.6 88.0  ONS/COMMENTS  PRIOR TO FEBRU AVAILABLE TIME DURING A UNIT OF AVAILABILIT PERIODS.  93.5 87.6	89.7 87.0 87.0 88.3 ARY 16, 1983 TO INCLUDE OUTAGE. THE Y AND CONSID	87.2 84.5 85.8 85.8 3, THE UTILIT PERIODS WHEN UTILITY NOW ERS THE SCRU	Y WAS I SCRU I CONF	CONSI BBER M ORMS T	672 DERING AINTEN O THE ( LABLE I	FGD SYS	577 STEM S PERFO DEFINITHESE	60.7 DRMED ITION
	** PROBLE  5A 5B SYSTEM  ** PROBLE  5A 5B SYSTEM	91.8 88.3 90.0 EMS/SOLUT: 92.3 90.5 91.4	ONS/COMMENTS  UNIT 5 WAS PLAY OUTAGE.  89.3 86.6 88.0  CONS/COMMENTS  PRIOR TO FEBRU AVAILABLE TIME DURING A UNIT OF AVAILABILIT PERIODS.  93.5 87.6 90.5	89.7 87.0 88.3 ARY 16, 1983 TO INCLUDE OUTAGE. THE Y AND CONSID 94.5 88.5 91.5	87.2 84.5 85.8 85.8 6, THE UTILIT PERIODS WHEN UTILITY NOW ERS THE SCRU	Y WAS I SCRU I CONF IBBER	CONSI BBER M ORMS T UNAVAI	672 DERING AINTEN. O THE ( LABLE I	FGD SY: ANCE WAS CORRECT DURING	577 STEM S PERFO DEFIN: THESE	CO.7  DRMED  ITION  55.4
	** PROBLE  5A 5B SYSTEM  ** PROBLE  5A 5B SYSTEM  ** PROBLE	91.8 88.3 90.0 EMS/SOLUT: 92.3 90.5 91.4	CONS/COMMENTS  UNIT 5 WAS PLAY OUTAGE.  89.3 86.6 88.0  CONS/COMMENTS  PRIOR TO FEBRU AVAILABLE TIME DURING A UNIT OF AVAILABILIT PERIODS.  93.5 87.6 90.5  CONS/COMMENTS  THE UTILITY RE DURING MARCH.	89.7 87.0 88.3 ARY 16, 1983 TO INCLUDE OUTAGE. THE Y AND CONSID 94.5 88.5 91.5	87.2 84.5 85.8 85.8 7 THE UTILITY PERIODS WHEN UTILITY NOW ERS THE SCRU 78.8 73.8 76.3	Y WAS I SCRU I CONF IBBER	CONSI BBER M ORMS T UNAVAI	672 DERING AINTEN. O THE ( LABLE I	FGD SY: ANCE WAS CORRECT DURING	577 STEM S PERFO DEFIN: THESE	60.7 DRMED ITION 55.4
3/83	** PROBLE  5A 5B SYSTEM  ** PROBLE  5A 5B SYSTEM  ** PROBLE	91.8 88.3 90.0 EMS/SOLUTE	CONS/COMMENTS  UNIT 5 WAS PLAY OUTAGE.  89.3 86.6 88.0  CONS/COMMENTS  PRIOR TO FEBRU AVAILABLE TIME DURING A UNIT OF AVAILABILIT PERIODS.  93.5 87.6 90.5  CONS/COMMENTS  THE UTILITY RE	89.7 87.0 88.3 ARY 16, 1983 TO INCLUDE OUTAGE. THE Y AND CONSID 94.5 88.5 91.5	87.2 84.5 85.8 85.8 6, THE UTILIT PERIODS WHEN UTILITY NOW ERS THE SCRU	Y WAS I SCRU I CONF IBBER	CONSI BBER M ORMS T UNAVAI	672 DERING AINTEN. O THE ( LABLE I	FGD SY: ANCE WAS CORRECT DURING	577 STEM S PERFO DEFIN: THESE	60.7 DRMED ITION 55.4

	MODULE AV	/AILABILI	TY OPERABILITY	RELIABILITY					BOILER HOURS		
	** PROBLE	MS/SOLUT	IONS/COMMENTS								
			THE UTILITY AT RING APRIL TO CHANGES IN THE	PROPER MAINT	ENANCE PERFO	RMED .					
5/83	5A	82.3	78.1 77.6	78.7	60.6						
	SYSTEM	74.6 78.4	77.6 77.8	78.2 78.4	60.2 60.4			744	<b>5</b> 78	450	49.3
	** PROBLE	MS/SOLUT	IONS/COMMENTS								
			THE UTILITY RE			WAS A	TTRIBU	red to	THE CLI	EANING	
			MAINTENANCE WO	RK ON MIST E	LIMINATOR PU	MPS A	LSO CAI	JSED O	JTAGE T	IME IN	MAY.
			A 72 HOUR OUTA POND. AIR HEA CONDITIONS IN	TER DRAINAGE							
6/83	5A	88.2	75.5 90.9	77.6	39.0						
	5B SYSTEM	96.5 92.4	90.9 8 <b>3.</b> 2	93.4 85.5	46.9 43.0			720	372	310	37.1
			IONS/COMMENTS								
			THE UTILITY REDURING JUNE.	PORTED THAT	NO MAJOR FGD	-RELA	TED PRO	OBLEMS	WERE E	HCOUNTE	ERED
7/07	5A		83.3								
//83				84.2	63.6						
//83	5B System	90.2	81.9					744	568	469	54.0
		90.2 89.0 94.1	81.9 82.6 83.8	82.7 <b>83.5</b> 88.0	62.5 63.0 67.3			744	568	469	54.0
	SYSTEM 5A 5B	90.2 89.0 94.1 91.3	81.9 82.6 83.8 84.1	82.7 83.5 88.0 88.4	62.5 63.0 67.3 67.6						
	SYSTEM 5A	90.2 89.0 94.1 91.3	81.9 82.6 83.8 84.1 83.9	82.7 83.5 88.0 88.4 88.2	62.5 63.0 67.3 67.6				568 598		
8/83	SYSTEM  5A 5B SYSTEM  5A	90.2 89.0 94.1 91.3 92.7	81.9 82.6 83.8 84.1 83.9	82.7 83.5 88.0 88.4 88.2	62.5 63.0 67.3 67.6 67.5						
8/83	SYSTEM  5A 5B SYSTEM  5A 5B	90.2 89.0 94.1 91.3 92.7 99.0 93.8	81.9 82.6 83.8 84.1 83.9 97.2 86.7	82.7 83.5 88.0 88.4 88.2 98.0 87.5	62.5 63.0 67.3 67.6 67.5 47.8 42.6				<b>5</b> 98	502	46.0
8/83	SYSTEM  5A 5B SYSTEM  5A 5B SYSTEM	90.2 89.0 94.1 91.3 92.7 99.0 93.8 96.4	81.9 82.6 83.8 84.1 83.9 97.2 86.7 91.9	82.7 83.5 88.0 88.4 88.2	62.5 63.0 67.3 67.6 67.5 47.8 42.6			744	<b>5</b> 98		46.0
8/83	SYSTEM  5A 5B SYSTEM  5A 5B SYSTEM	90.2 89.0 94.1 91.3 92.7 99.0 93.8 96.4	81.9 82.6 83.8 84.1 83.9 97.2 86.7	82.7 83.5 88.0 88.4 88.2 98.0 87.5 92.7	62.5 63.0 67.3 67.6 67.5 47.8 42.6 45.2	)-RELA	TED PR	744 720	<b>5</b> 98 354	502 326	46.0 34.0
8/83	SYSTEM  5A 5B SYSTEM  5A 5B SYSTEM	90.2 89.0 94.1 91.3 92.7 99.0 93.8 96.4	81.9 82.6 83.8 84.1 83.9 97.2 86.7 91.9	82.7 83.5 88.0 88.4 88.2 98.0 87.5 92.7	62.5 63.0 67.3 67.6 67.5 47.8 42.6 45.2			744 720	<b>5</b> 98 354	502 326	46.0 34.0
8/83 9/83	SYSTEM  5A 5B SYSTEM  5A 5B SYSTEM  ** PROBLI	90.2 89.0 94.1 91.3 92.7 99.0 93.8 96.4 EMS/SOLUT	81.9 82.6 83.8 84.1 83.9 97.2 86.7 91.9 TIONS/COMMENTS THE UTILITY REDURING THE PER	82.7 83.5 88.0 88.4 88.2 98.0 87.5 92.7	62.5 63.0 67.3 67.6 67.5 47.8 42.6 45.2 NO MAJOR EGE THROUGH SEPT			744 720	<b>5</b> 98 354	502 326	46.0 34.0
8/83	SYSTEM  5A 5B SYSTEM  5A 5B SYSTEM  ** PROBLE	90.2 89.0 94.1 91.3 92.7 99.0 93.8 96.4 EMS/SOLUT	81.9 82.6 83.8 84.1 83.9 97.2 86.7 91.9 TONS/COMMENTS THE UTILITY REDURING THE PER 98.0 94.7	82.7 83.5 88.0 88.4 88.2 98.0 87.5 92.7 PORTED THAT FOOD OF JULY 98.0 94.7	62.5 63.0 67.3 67.6 67.5 47.8 42.6 45.2 NO MAJOR EGE THROUGH SEPT			744 720 DBLEMS	598 354 WERE E	502 326 NCOUNTE	46.0 34.0 ERED
8/83 9/83	SYSTEM  5A 5B SYSTEM  5A 5B SYSTEM  ** PROBLE	90.2 89.0 94.1 91.3 92.7 99.0 93.8 96.4 EMS/SOLUT	81.9 82.6 83.8 84.1 83.9 97.2 86.7 91.9 TIONS/COMMENTS THE UTILITY REDURING THE PER 98.0 94.7 96.3	82.7 83.5 88.0 88.4 88.2 98.0 87.5 92.7	62.5 63.0 67.3 67.6 67.5 47.8 42.6 45.2 NO MAJOR EGE THROUGH SEPT			744 720	598 354 WERE E	502 326 NCOUNTE	46.0 34.0
8/83 9/83	SYSTEM  5A 5B SYSTEM  5A 5B SYSTEM  ** PROBLE	90.2 89.0 94.1 91.3 92.7 99.0 93.8 96.4 EMS/SOLUT	81.9 82.6 83.8 84.1 83.9 97.2 86.7 91.9 TIONS/COMMENTS THE UTILITY REDURING THE PER 98.0 94.7 96.3	82.7 83.5 88.0 88.4 88.2 98.0 87.5 92.7 PORTED THAT FOOD OF JULY 98.0 94.7 96.3	62.5 63.0 67.3 67.6 67.5 47.8 42.6 45.2 NO MAJOR FGE THROUGH SEPT 46.9 45.3 46.1	TEMBER	1983.	744 720 DBLEMS 744	598 354 WERE E1	502 326 NCOUNTE	46.0 34.0 ERED
8/83 9/83	SYSTEM  5A 5B SYSTEM  5A 5B SYSTEM  ** PROBLI	90.2 89.0 94.1 91.3 92.7 99.0 93.8 96.4 EMS/SOLUT	81.9 82.6 83.8 84.1 83.9 97.2 86.7 91.9 TIONS/COMMENTS THE UTILLITY REDURING THE PER 98.0 94.7 96.3 TIONS/COMMENTS	82.7 83.5 88.0 88.4 88.2 98.0 87.5 92.7 PORTED THAT IOD OF JULY 98.0 94.7 96.3	62.5 63.0 67.3 67.6 67.5 47.8 42.6 45.2 NO MAJOR EGD THROUGH SEPT 46.9 45.3 46.1	TEMBER	1983.	744 720 DBLEMS 744	598 354 WERE E1	502 326 NCOUNTE	46.0 34.0 ERED
8/83 9/83	SYSTEM  5A 5B SYSTEM  5A 5B SYSTEM  ** PROBLI	90.2 89.0 94.1 91.3 92.7 99.0 93.8 96.4 EMS/SOLUT	81.9 82.6 83.8 84.1 83.9 97.2 86.7 91.9 TIONS/COMMENTS THE UTILITY REDURING THE PER 98.0 94.7 96.3	82.7 83.5 88.0 88.4 88.2 98.0 87.5 92.7 PORTED THAT FOOD OF JULY 98.0 94.7 96.3	62.5 63.0 67.3 67.6 67.5 47.8 42.6 45.2 NO MAJOR FGE THROUGH SEPT 46.9 45.3 46.1	TEMBER	1983.	744 720 DBLEMS 744	598 354 WERE E1	502 326 NCOUNTE	46.0 34.0 ERED

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT ANNUAL OUTAGES OCCURRED DURING NOVEMBER FOR UNITS 5 AND 6.

12/83	A	30.2	59.2	67.1	19.5			
	В	31.3	60.8	69.0	20.0			
	SYSTEM	30.8	60.0	68.1	19.8	744	245	147 17.9

#### ** PROBLEMS/SOLUTIONS/COMMENTS

FGD SYSTEM OUTAGE TIME DURING DECEMBER WAS DUE IN PART TO THE LOSS OF A LIME FEED LINE AND FROZEN WATER LINES ON THE SLAKERS.

THE UNAVAILABILITY OF THE SLUDGE TREATMENT FACILITY CONTRIBUTED TO FGD SYSTEM DOWN TIME DURING THE MONTH.

A LOCALIZED ABSORBER RUBBER LINER FAILURE ALSO CONTRIBUTED TO FGD SYSTEM OUTAGE TIME DURING DECEMBER.

1/84	A	94.1	87. <b>8</b>	89.7	46.6				
	В	98.1	95.4	97.4	50.7				
	SYSTEM	96.1	91.6	93.5	48.7	744	395	362	35.0

#### ** PROBLEMS/SOLUTIONS/COMMENTS

ABSORBER RUBBER LININGS WERE REPAIRED DURING THE MONTH.

MIST ELIMINATOR AND RECYCLE SPRAY NOZZLES WERE CLEANED DURING JANUARY.

A POWER SUPPLY FAILURE AND COMPUTER-RELATED PROBLEMS ACCOUNTED FOR OUTAGE TIME IN JANUARY.

2/84	5A	98.9	70.4	81.3	20.5				
	5B	96.0	68.5	79.0	20.0				
	SYSTEM	97.4	69.5	80.1	20.3	696	203	141 1	17.5

#### ** PROBLEMS/SOLUTIONS/COMMENTS

POOR LIME QUALITY ACCOUNTED FOR OUTAGE TIME DURING FEBRUARY.

A POWER FAILURE AT THE SLUDGE TREATMENT PLANT CONTRIBUTED TO DOWN TIME.

ABSORBER LINER FAILURE ACCOUNTED FOR ADDITIONAL OUTAGE TIME IN FEBRUARY.

3/84	A	98.3	96.4	98. <b>0</b>	85.8				
		99.6	97.9	99.5	87.1				
	SYSTEM	98.9	97.1	98.8	86.4	744	662	643	64.4

# ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE UNIT WAS OUT OF SERVICE 14 HOURS DUE TO FAULTY DAMPERS.

RECYCLE TANK AGITATOR PROBLEMS WERE REPORTED DURING MARCH.

4/84	5A 5B SYSTEM	100.0 98.5 99.2	99.0 97.0 98.0	100.0 97.9 98.9	72.4 70.8 71.6	720	526	516	51.0
5/84	5A 5B System	99.9 99.6 99.7	99.7 99.5 99.6	99.7 99.5 99.6	79.6 79.4 79.5	744	594	592	58.0

				PERFORMAI	NCE DATA						
PERIOD	MODULE	AVAILABILITY				% REMO	VAL	PER	BOILER HOURS	FGD HOURS	CAP. FACTOR
6/84	5A	98.3	96.6	97.9	81.8						
	5B	99.3	<b>9</b> 7.9	99.3	82.9						
	SYSTEM	98.8	97.3	98.6	82.3			720	609	593	55.5
7/84	5A	93.5	96.7	99.3	36.4						
	<b>5</b> B	93.5	96.7	99.3	36.4						
	SYSTEM	93.5	96.7	99.3	36.4			744	280	271	24.5

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD RELATED PROBLEMS WERE ENCOUNTERED DURING THE PERIOD OF APRIL THROUGH JULY, 1984.

8/84	SYSTEM	744
9/84	SYSTEM	720

### ** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR AUGUST AND SEPTEMBER 1984.

# SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COLUMBUS & SOUTHERN OHIO ELEC COMPANY NAME CONESVILLE PLANT NAME UNIT NUMBER CONESVILLE CITY OHIO STATE D REGULATORY CLASSIFICATION 43. ( .100 LB/MMBTU) 516. ( 1.200 LB/MMBTU) 301. ( .700 LB/MMBTU) PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J 1890 NET PLANT GENERATING CAPACITY - MW 405 373 GROSS UNIT GENERATING CAPACITY - MW NET UNIT GENERATING CAPACITY WO/FGD - MW EQUIVALENT SCRUBBED CAPACITY NET UNIT GENERATING CAPACITY W/FGD - MW 380 350 ** UNIT DATA - BOILER AND STACK COMBUSTION ENGINEERING BOILER SUPPLIER PULVERIZED COAL BOILER TYPE CYCLING BOILER SERVICE LOAD DESIGN BOILER FLUE GAS FLOW - CU.M/S BOILER FLUE GAS TEMPERATURE - C STACK HEIGHT - M 596.95 (1265000 ACFM) 146.7 ( 296 F) 244. ( 800 FT) 244. CONCRETE STACK SHELL STACK TOP DIAMETER - M 7.9 ( 26.0 FT) ** FUEL DATA FUEL TYPE COAL
BITUMINOUS
05037. ( 10850 BTU/LB) COAL FUEL GRADE AVERAGE HEAT CONTENT - J/G RANGE HEAT CONTENT - BTU/LB 14.90 AVERAGE ASH CONTENT - % 14.90 10.0-24.0 7.50 5.0-18.0 4.50 4.2-5.1 .01 0.01-0.11 RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - % RANGE MOISTURE CONTENT - %
AVERAGE SULFUR CONTENT - % RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - % *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER 0 TYPE NONE ** FSP NUMBER 1 NUMBER OF SPARES 0 TYPE COLD SIDE SUPPLIER RESEARCH-COTTRELL INLET FLUE GAS CAPACITY - CU.M/S 657.8 (1393893 ACFM) 146.7 ( 296 F) .5 ( 2. IN-H2O) 99.6 INLET FLUE GAS TEMPERATURE - C PRESSURE DROP - KPA PARTICLE REMOVAL EFFICENCY - X ** PARTICLE SCRUEBER NUMBED GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL N/A LINER GENERIC MATERIAL N/A LINER SPECIFIC MATERIAL N/A GAS CONTACTING DEVICE TYPE N/A

*** FGD SYSTEM

```
** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                               THROWAWAY PRODUCT
   SO2 REMOVAL MODE
                                               WET SCRUBBING
   PROCESS TYPE
                                                LIME
   PROCESS ADDITIVES
                                               MAG
   SYSTEM SUPPLIER
                                               AIR CORRECTION DIVISION, UOP
   A-E FIRM
                                               BLACK & VEATCH
   DEVELOPMENT LEVEL
                                               FULL SCALE
   NEW/RETROEIT
                                               NFM
                                                 99.65
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - %
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                   89.50
   ENERGY CONSUMPTION - %
                                                    1.7
   CURRENT STATUS
                                                 1
   COMMERCIAL START-UP
                                                 7/78
   INITIAL START-UP
                                                 6/78
   CONTRACT AWARDED
                                                10/74
** DESIGN AND OPERATING PARAMETERS
   OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                  280.0
** QUENCHER/PRESATURATOR
   NUMBER
    TYPE
                                                SPRAY CHAMBER
    SUPPLIER
                                                AIR CORRECTION DIVISION, UOP
    INLET GAS TEMPERATURE - C
                                                  141.1
                                                              ( 286 F)
    L/G RATIO - L/CU. M
                                                                   .6 GAL/1000 ACFM)
                                                     1
                                                               ſ
                                               HIGH ALLOY
    CONSTRUCTION MATERIAL GENERIC TYPE
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                IRON BASE/NICKEL-CHROMIUM-COPPER-MOLYBDENUM
** ABSORBER
   NUMBER
   NUMBER OF SPARES
                                                 Λ
    GENERIC TYPE
                                                PACKED TOWER
    SPECIFIC TYPE
                                               MOBILE BED PACKING
    TRADE NAME/COMMON TYPE
                                                TURBULENT CONTACT ABSORBER
                                                AIR CORRECTION DIVISION, UOP
    SUPPLIER
                                                45.0 X 17.5 X 79.5
    DIMENSIONS
                FT
    SHELL GENERIC MATERIAL
                                                CARBON STEEL
    SHELL SPECIFIC MATERIAL
                                                AISI 1110
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                                N/A
    LINER GENERIC MATERIAL
                                                ORGANIC
    LINER SPECIFIC MATERIAL
                                                SYNTHETIC RUBBER
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                                NEOPRENE LS-576
    GAS CONTACTING DEVICE TYPE
                                                GRID CAGES
   NUMBER OF CONTACTING ZONES
                                                 1
                                                 1988.
    LIQUID RECIRCULATION RATE - LITER/S
                                                               (31560 GPM)
                                                               ( 49.3 GAL/1000 ACF)
    L/G RATIO - L/CU.M
                                                    6.6
    GAS-SIDE PRESSURE DROP - KPA
                                                    2.0
                                                               ( 8.1 IN-H20)
    SUPERFICAL GAS VELOCITY - M/SEC
                                                    4.0
                                                               ( 13.1 FT/S)
                                                  301.81
    INLET GAS FLOW - CU. M/S
                                                               ( 639568 ACFM)
   INLET GAS TEMPERATURE - C
                                                  51.7
                                                               ( 125 F)
    SO2 REMOVAL EFFICIENCY - %
                                                   92.0
    PARTICLE REMOVAL EFFICENCY - %
                                                   99.6
** MIST ELIMINATOR
                                                PRIMARY COLLECTOR
   PRE-MIST ELIMINATOR/MIST ELIMINATOR
   NUMBER PER SYSTEM
                                                 2
   NUMBER OF SPARES PER SYSTEM
                                                 0
   NUMBER PER MODULE
                                                 1
   GENERIC TYPE
                                                IMPINGEMENT
   SPECIFIC TYPE
                                                BAFFLE
   TRADE NAME/COMMON TYPE
                                                CLOSED VANE
                                                HORIZONTAL
   CONFIGURATION
   NUMBER OF STAGES
                                                    2
   NUMBER OF PASSES PER STAGE
   FREEBOARD DISTANCE - M
                                                    3.05
                                                               (10.0 FT)
                                                               ( 4.5 IN)
   DISTANCE BETHEEN STAGES - CM
                                                   11.43
   DISTANCE BETWEEN VANES - CM
                                                    5.1
                                                               ( 2.00 IN)
                DEGREES
                                                  90
   VANE ANGLES
   PRESSURE DROP - KPA
                                                     . 5
                                                               ( 1.9 IN-H20)
```

( 10.0 FT/S) 3.0 SUPERFICAL GAS VELOCITY - M/S CONSTRUCTION MATERIAL GENERIC TYPE ORGANIC FIBER-REINFORCED POLYESTER CONSTRUCTION MATERIAL SPECIFIC TYPE RECLAIMED WASH WATER SOURCE CONTINUOUS WASH FREQUENCY ( 1000 GAL/MIN) 63.1 WASH RATE LS ** REHEATER NONE GENERIC TYPE N/A SPECIFIC TYPE N/A TRADE NAME/COMMON TYPE NONE CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE N/A ** FANS 2 NUMBER NUMBER OF SPARES 0 CENTRIFUGAL DESIGN GREEN FAN SUPPLIER TINU FUNCTION FORCED DRAFT APPLICATION DRY SERVICE ( 850000 ACFM) 401.11 FLUE GAS FLOW RATE - CU.M/S ( 296 F) FLUE GAS TEMPERATURE C 146.7 ( 2.0 IN-H20) PRESSURE DROP - KPA .6 CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL ** DAMPERS NUMBER 2 SHUT-OFF FUNCTION GUILLOTINE GENERIC TYPE CONSTRUCTION MATERIAL GENERIC TYPE HIGH ALLOY NICKEL BASE/CHROMIUM-IRON-MOLYBDENUM CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE NONE NAA LINER SPECIFIC MATERIAL TYPE ** DAMPERS NUMBER 2 SHUT-OFF FUNCTION GUILLOTINE GENERIC TYPE CONSTRUCTION MATERIAL GENERIC TYPE HIGH ALLOY CONSTRUCTION MATERIAL SPECIFIC TYPE NICKEL BASE/CHROMIUM-IRON-MOLYBDENUM NONE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE N/A ** DAMPERS 2 NUMBER FUNCTION CONTROL GUILLOTINE & LOUVER GENERIC TYPE CONSTRUCTION MATERIAL GENERIC TYPE HIGH ALLOY CONSTRUCTION MATERIAL SPECIFIC TYPE NICKEL BASE/CHROMIUM-IRON-MOLYBDENUM LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DUCTHORK INLET LOCATION SHELL GENERIC MATERIAL TYPE CARBON STEEL SHELL SPECIFIC MATERIAL TYPE HIGH STRENGTH LOW ALLOY [HSLA] LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DUCTWORK OUTLET TO DAMPER LOCATION SHELL GENERIC MATERIAL TYPE CARBON STEEL SHELL SPECIFIC MATERIAL TYPE HIGH STRENGTH LOW ALLOY [HSLA] LINER GENERIC MATERIAL TYPE ORGANIC LINER SPECIFIC MATERIAL TYPE GLASS FLAKE-FILLED POLYESTER ** DUCTWORK LOCATION OUTLET BEYOND DAMPER

CARBON STEEL

SHELL GENERIC MATERIAL TYPE

SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE
HIGH STRENGTH LOW ALLOY [HSLA]
INORGANIC
CHEMICALLY-BONDED CONCRETE

### ** DUCTWORK

LOCATION BYPASS

SHELL GENERIC MATERIAL TYPE CARBON STEEL

SHELL SPECIFIC MATERIAL TYPE HIGH STRENGTH LOW ALLOY (HSLA)

LINER GENERIC MATERIAL TYPE NONE

LINER SPECIFIC MATERIAL TYPE N/A

SLAKER

PASTE

WALLACE & TIERNAN

N/A

5

NUMBER

1

2

### ** REAGENT PREPARATION EQUIPMENT

FUNCTION
DEVICE
DEVICE TYPE
MANUFACTURER
NUMBER

### ** TANKS

SERVICE
-----ABSORGER RECYCLE
RECLAIMED WATER
REAGENT PREP PRODUCT
HIST FLIMINATOR WASH

### ** PUMPS

SERVICE NUMBER -----ABSORBER RECIRCULATION 10 LIME SLURRY TRANSFER 2 SLURRY MAKEUP 3 RECYCLE TANK DRAWOFF 4 MIST ELIMINATOR WASH 4 RECLATM WATER 2 THICKENER UNDERFLOW ***

### ** SOLIDS CONCENTRATING/DEWATERING

DEVICE
NUMBER
NUMBER OF SPARES
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
BELT GENERIC MATERIAL TYPE
BELT SPECIFIC MATERIAL TYPE
BELT SPECIFIC MATERIAL TYPE
FEED STREAM SOURCE
FEED STREAM CHARACTERISTICS
OUTLET STREAM CHARACTERISTICS
OUTLET STREAM DISPOSITION
OVERFLOW STREAM DISPOSITION

### ** SOLIDS CONCENTRATING/DEWATERING

DEVICE
NUMBER
NUMBER OF SPARES
DIMENSIONS FT
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE
FEED STREAM SOURCE
FEED STREAM CHARACTERISTICS
OUTLET STREAM CHARACTERISTICS
OUTLET STREAM DISPOSITION
OVERFLOW STREAM DISPOSITION

## VACUUM FILTER

3
1
CARBON STEEL
AISI 1110
ORGANIC
POLYPROPYLENE
THICKENER UNDERFLOW
30% SOLIDS
50% SOLIDS
TO IUCS FROCESS
TO RECLAIMED WATER TANK

### THICKENER

2
0
145.0 DIA X 16.0
CARBON STEEL
AISI 1110
ORGANIC
EPOXY
ABSORBER BLEED
7-12% SOLIDS
30% SOLIDS
TO JUCS THICKENE

TO JUCS THICKENER & THEN TO VACUUM FILTER TO RECLAIMED WATER TANK

### *** SLUDGE

COLUMBUS & SOUTHERN OHIO ELEC: CONESVILLE 6 (CONT.)

** TREATMENT

METHOD DEVICE

PROPRIETARY PROCESS

INLET QUALITY - %

FIXATION PUG MILL

CONVERSION SYSTEMS [POZ-O-TEC]

50.0

** DISPOSAL

NATURE TYPE

LOCATION

SITE TRANSPORTATION METHOD

SITE TREATMENT

SITE DIMENSIONS

FINAL LANDFILL ON-SITE

PIPELINE/CONVEYED

NONE

80 ACRES/50 FT

** PROCESS CONTROL AND INSTRUMENTATION

CHEMICAL PARAMETERS PHYSICAL VARIABLES CONTROL LEVELS MONITOR LOCATION PROCESS CONTROL MANNER PROCESS CHEMISTRY MODE

PH RECYCLE TANK LEVEL

OUTLET PH 5.5-6.3; RECYCLE PH 7.0-7.5

SLURRY DISCHARGE FROM MODULE

AUTOMATIC

FEEDBACK

** WATER BALANCE

WATER LOOP TYPE

MAKEUP WATER ADDITION - LITERS/S

CLOSED

( 500 GPM) 31.5

** CHEMICALS AND CONSUMPTION

FUNCTION NAME PRINCIPAL CONSTITUENT SOURCE/SUPPLIER CONSUMPTION UTILIZATION - % POINT OF ADDITION

ABSORBENT LIME 90-95% CAO, 3-8% MGO

DRAVO 16 TPH 90.0 SLAKER

** FGD SPARE CAPACITY INDICES

ABSORBER - %

.0

** FGD SPARE COMPONENT INDICES

ABSORBER

. 0

				DED FODMAR	NCE BATA	 			
		AVAILABILITY				PER	BOILER	FGD	CAP.
6/78	A B SYSTEM	56.0 44.0 50.0	49.0 33.0 41.0	51.0 34.0 42.5	42.0 30.0 36.0	720	524	174	

### ** PROBLEMS/SOLUTIONS/COMMENTS

INITIAL OPERATIONS OF THE CONESVILLE 6 FGD SYSTEM BEGAN IN JUNE.

CONTROL OF THE LOUVERED DAMPER OF THE BYPASS SYSTEM WAS LOST. THE RESULT WAS BACK PRESSURE BUILDUP THAT AUTOMATICALLY SHUT DOWN THE BOILER.

SCRUBBER CONTROLS WERE NOT OPERATING PROPERLY AND NEEDED ADJUSTMENT.

7/78 A 83.0 37.0 63.0 25.0 В 70.0 19.0 33.0 13.0 SYSTEM 76.5 28.0 48.0 19.0

744 502 141

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE LOUVERED DAMPER PROBLEM CONTINUED.

THE FRP TRANSFER LINE FROM THE THICKENER TO THE IUCS SYSTEM RUPTURED AS A

	MODULE AVA	ILABILI.	TY OPERABILITY R		CE DATA UTILIZATION			PER E			
			RESULT OF WATE	R HAMMER IN	THE LINE A	DAH D	TO BE	REPAIR	D.		
8/78			50.0 60.0	66.0							
			55.0					744	642	354	
	** PROBLEM	S/SOLUT:	IONS/COMMENTS								
			PROBLEMS WERE THAT THIS IS T				_	THE UT:	LITY F	REPORTE	ED .
			PROBLEMS WERE REPORTED THAT							IE UTIL	LITY
9/78		55.0		53.0	49.0						
	B System	69.0 62.0	<b>5</b> 5.0 52.5	57.0	54.0			720	706	372	
			IONS/COMMENTS								
			A PROBLEM AREA	WAS THE PL	.UGGING OF TI	HE LIM	E SLURI	RY FEED	LINES		
			BYPASS DAMPER	CONTROL PRO	BLEMS CONTI	NUED TI	HROUGH	SEPTEME	BER.		
10/78	A	98.0	29.0	30.0	24.0						
	B SYSTEM	37 N	35.0	36.0 33.0	29.0			744	407	100	
	•			33.0	20.5			/44	603	199	
	** PRUBLEM	3/30[0]	IONS/COMMENTS								
			PROBLEMS WITH PLANS TO REPLA						D. TH	łE UTII	LITY
11/78	A	26.0	3.0	3.0	2.0						
	D	26.0	9.0 6.0	9.0	8.0			720	600	36	
	** PROBLEM	S/SOLUT	IONS/COMMENTS								
			LIME TRANSFER	BAGHOUSE SH	IAKER PROBLEI	MS WER	E EXPE	RIENCED			
			THE THICKENER	RAKE MOTOR	BURNED OUT	AND HAI	о то в	E REWOUT	٠O.		
12/78	A	34.8	26.3	26.8	24.2						
	B SY <b>S</b> TEM	26.6 30.7	19.0 22.6	19.3 23.0	17.5 20.8			744	672	155	
								744	6/2	155	
1/79	A B	5.0 .0	2.0	2.0 .0	2.0						
	SYSTEM	2.5	.0 1.0	1.0	.0 1.0			744	730	8	
	** PROBLEM	S/SOLUT	IONS/COMMENTS								
			FREEZE UPS WERE	E A SERIOUS	PROBLEM DUR	ING TH	E DECE	MBER-JAI	NUARY I	PERIOD.	•
2/79	SYSTEM	.0	.0	.0	.0			672	629	0	
2/79	-		.0 IONS/COMMENTS	.0	.0			672	629	0	
2/79	-			DID NOT OPE	RATE DURING	FEBRU	ARY DU		-		<b>4EATHE</b> R

COLUMBUS & SOUTHERN OHIO ELEC: CONESVILLE 6 (CONT.)

				PERFORMA	NCE DATA						
		AVAILABILITY				% RE	MOVAL	PER	BOILER HOURS	FGD	CAP.
	В	32.0	28.0	29. <b>0</b>	25.0						
	SYSTEM	37.5	32.5	34.0	29.0			744	664	216	
4/79	A	82.0	79.0	79.0	78.0						
	В	72.0	59. <b>0</b>	59.0	58.0						
	SYSTEM	77.0	69.0	69.0	68.0			720	711	489	
5/79	SYSTEM	100.0			.0			744	0	0	.0

### ** PROBLEMS/SOLUTIONS/COMMENTS

REPAIRS WERE MADE TO THE SEAL BETWEEN THE THICKENER BASE AND SIDEWALL.

THE BOILER DID NOT OPERATE DURING MAY DUE TO A SCHEDULED ANNUAL OUTAGE.

6/79	A	43.0	37.0	39.0	27.0			
	В	49.0	49.0	52.0	31.0			
	SYSTEM	46.0	43.0	45.5	29.0	720	433	209

### ** PROBLEMS/SOLUTIONS/COMMENTS

FLYASH CONVEYING PROBLEMS RESULTED IN ABOUT A TWO DAY OUTAGE.

PLUGGED PH LINES WERE A PROBLEM DURING THIS PERIOD.

7/79	A B System	83.9 88.7 86.3	29.5 41.2 35.4	29.7 41.4 35.6	22.0 30.8 26.4	744	554	196
8/79	A B SYSTEM	76.2 77.6 76.9	40.8 42.6 41.7	40.8 42.6 41.7	40.8 42.6 41.7	744	744	310
9/79	A B System	87.6 86.5 87.0	58.5 55.5 57.0	57.4 56.2 56.8	54.4 53.3 53.9	720	681	388
10/79	A B System	75.9 43.1 59.5	66.2 23.6 44.9	66.5 23.7 45.1	63.3 22.6 43.0	744	713	320
11/79	A B SYSTEM	67.0 52.0 59.5	58.0 49.0 53.5	58.0 49.0 53.5	48.0 41.0 44.5	72 <b>0</b>	599	320
12/79	A B SYSTEM	84.0 91.0 87.5	76.0 87.0 81.5	76.0 87.0 81.5	76.0 87.0 81.5	744	744	606

### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE LAST HALF OF 1979 THE UNIT EXPERIENCED PROBLEMS WITH THE LIME BLOHER COMPRESSOR MOTOR.

CAVITATION WAS SITED IN THE SLUDGE PUMP.

THE FLYASH CONVEYOR SYSTEM CAUSED PROBLEMS DURING THE LATTER HALF OF THE YEAR.

PLUGGING IN THE REAGENT CIRCULATION SYSTEMS WAS ENCOUNTERED.

THERE WERE PROBLEMS WITH THE GUIDE BARS AND SEALS IN THE INLET DAMPER DURING THE LAST HALF OF 1979.

PERIOD	MODULE	AVAILABILI	TY OPERABILITY	RELIABILITY		% REI	MOVAL PART.	PER HOURS	BOILER HOURS		
1/80	A	88.0	74.0 78.0	74.0	74.0 78.0						
	B	89.0	78.0	78. <b>0</b>	78.0						
	SYSTEM	89.0	76.0	76.0	76.0			744	744	566	73.9
	** PROE	BLEMS/SOLUT	IONS/COMMENTS								
			NO MAJOR FGD	SYSTEM RELAT	ED PROBLEMS I	WERE RI	EPORTE	D FOR .	JANUARY	•	
2/80	A	87.0	75.0	78.0	69.0						
	В	92.0	81.0	85.0	75.0						
	SYSTEM	90.0	78.0	82.0	72.0			6 96	648	503	70.8
	** PRO	BLEMS/SOLUT	IONS/COMMENTS								
			IN FEBRUARY,	MIST ELIMINA	TOR NOZZLE P	LUGGIN	occu	RRED CA	AUSING	SOME OL	JTAGE
3/80	Δ	93.0	69.0	69.0	15.0						
	B	94.0	69.0 76.0	69.0 76.0	15.0 16.0						
		94.0	73.0	73.0	16.0			744	160	117	17.6
	** PRO	BLEMS/SOLUT	IONS/COMMENTS								
			THE BOILER WE REMAINED OUT						SPECTIO	DHA H	
4/80	A	98.8	25.6	29.4	11.1						
	В	98.9	54.2	62.1	23.5						
	SYSTEM		40.1		17.4			720	312	125	19.8
	** PRO	BLEMS/SOLUT	IONS/COMMENTS								
			CONTINUOUS PR						ND NOZZ	LES	
5/80	A	96.9	58.3	63.8	55.0						
	SYSTEM	96.5	33.8 46.1	50.4	43.4			744	701	323	39.1
	** PRO	BLEMS/SOLUT	IONS/COMMENTS								
			CONTROL AND I BLE FOR SOME			THAT DI	EVELOP	ED IN 1	MAY WER	E RESPO	ONSI-
6/80	A	97.1	73.6	73.4	73.1						
	В	97.1	50.5	50.3	50.1						
	SYSTEM	97.1	62.1	61.9	61.7			720	715	444	52.5
	** PROE	BLEMS/SOLUT	IONS/COMMENTS								
			THE MAJORITY CAUSES (IUCS								L
7/80	A	96.0	85.1	85.9	82.7						
., 50	В	99.1	89.1	89.9	86.6						
	SYSTEM		87.1	87.9	84.6			744	722	630	61.7
	- · J · • · ·	, <b>.</b>	<u>.</u>	- · • /	- · • •			,			
	** PRO	BLEMS/SOLUT	IONS/COMMENTS								

THE FGD SYSTEM EXPERIENCED PROCESS CONTROL PROBLEMS DURING JULY.

PROBLEMS WITH LEAKING INLET DAMPER SEALS ALSO OCCURRED DURING JULY.

COLUMBUS & SOUTHERN OHIO ELEC: CONESVILLE 6 (CONT.)

				PERFORMAN	CE DATA						
PERIOD	MODULE	AVAILABILITY			UTILIZATION	S02	PART.	HOURS	HOURS	HOURS	CAP. FACTOR
								4			
8/80	A	90.2	65.4	67.3	30.1						
	R	97.4	85.5	88.0	39.4 <b>3</b> 4.7						
	SYSTEM	93.8	75.5	77.6	34.7			744	343	259	28.3
	** PROB	BLEMS/SOLUTION	NS/COMMENTS								
					PROBLEMS WER			ED WITH	I THE RI	ECLAIM	WATER
9/80	A B	93.6	88.2	88.5 91.0	87.8						
	В	94.2	90.7	91.0	90.3						
	SYSTEM	93.9	89.5	89.8	89.0			720	716	641	72.6
	** PRO	SLEMS/SOLUTIO	NS/COMMENTS								
		T	HE INLET DAM	PER SEAL PRO	BLEM CONTINUE	D THR	OUGH A	UGUST A	AND SEP	TEMBER.	•
		E:	XTERNAL PROB	LEMS WERE EXI	PERIENCED WIT	н тне	IUCS	SYSTEM	•		
10/80	Δ	89.2	72.n	72.6	64.9						
10,00	A B	94.1	87.6	72.6 88.3	78.9						
	SYSTEM	91.7	79 A	80.5	71.9			744	670	535	57 2
								, , , ,	070	939	37.2
11/80	A	99.6 98.2	92.9	91.1	55.4						
	В	98.2	81.5	79.9	48.6						
	SYSTEM	98.9	87.3	85.5	51.9			720	429	374	43.1
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
				EPORTED THAT	NO MAJOR FGD	-RELA	TED PR	OBLEMS	WERE SI	NCOUNTE	ERED
12/80	Δ	86.0	84 0	84.0	84 0						
12,00	B	87.6	74.7	76.7	74.7						
	_	86.8						744	744	744	79.1
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
		ים	URING DECEMB	ER SYSTEM AV	AILABILITY WA	S LOW	DUE T	O NECES	SSARY R	EPAIRS	
			O THE RECLAI	M WATER TANK	•						
1/81		97.6	92.7	92.7	92.7						
	В	98.4	90.5	90.4	90.4						
	SYSTEM	97.9	92.0	91.5	91.5			744	744	681	79.0
2/81	A	89.7	81.0	81.3	74.7						
	В	95.2	89.2	89.6	82.3						
	SYSTEM		85.0	85.4	78.4			672	620	528	75.4
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
				Y AND FEBRUAI ENCOUNTERED	RY THE UTILIT	Y REP	ORTED	THAT NO	MAJOR	FG0-RI	ELATED
3/81	A	74.7	04.4	00.0	F.C						
2/ OT	В		96.6	98.0	58.9						
	SYSTEM	75.0 74.9	97.5 97.0	99.0 98.5	59.4 59.1			744	453	440	57.7
				, 5.5	J / 8 L			, 75	793	770	27
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								

THE MAJORITY OF OUTAGE TIME DURING MARCH WAS THE RESULT OF LOW BOILER LOAD OR A LACK OF POWER DEMAND.

PERIOD	MODULE			PERFORMANC RELIABILITY U			PER	BOILER		
				TH SOME MINOR EQUIPMENT. NO						
4/81		53.3	95.0	99.1	31.9					
	В		100.0		33.6					
	SYSTEM	51.4	97.5	99.5	32.8		720	242	236	
	** PROB	LEMS/SOLUTI	ONS/COMMENTS							
				UNIT WAS OUT I		FOR A SCHEDU	JLED OL	JTAGE.	THE UN	IT
5/81	A	99.6		100.0	83.3					
	В	99.6	100.0	100.0	83.3					
	SYSTEM	99.6	100.0	100.0	83.3		744	620	620	
6/81	A	99.2	100.0	100.0	90.0					
	В	99.2	100.0	100.0 100.0	90.0					
	SYSTEM	99.2	100.0	100.0	90.0		720	648	648	
	** PROB	LEMS/SOLUTI	ONS/COMMENTS							
			THE UTILITY R DURING MAY AN	EPORTED THAT N D JUNE.	O MAJOR OPE	ERATIONAL PRO	BLEMS	WERE E	NCOUNTE	RED
7/81	A	99.6	100.0	100.0	73.9					
	В	99.2	100.0	100.0	73.9					
	SYSTEM	99.4	100.0	100.0	73.9		744	550	550	
8/81	A	99.0	90.0	94.0	74.0					
	В	98.0	89.0	92.0	73.0					
	SYSTEM	98.5	89.5	93.0	73.5		744	607	547	
9/81	A	100.0	85.0	94.0	35.0					
	В	89.0			36.0					
	SYSTEM	94.5	86.0	95.5	35.5		720	297	256	
	** PROE	BLEMS/SOLUTI	ONS/COMMENTS							
			FAILED DUE TO	DUCT CORROSIO INADEQUATE ST TO INCONEL OR	RENGTH OF 1	THE SUPPORTIN	G MESH			
			THE UNIT IS N	MOVED FROM SER OT EXPECTED TO ERIOD WILL BE	BE BROUGHT	T BACK ON LI	4E UNT	L DECE	MBER.	MAND.
10/81	A	100.0	.0	.0	.0					
	В	100.0	.0	.0	. 0		7//		•	
	SYSTEM	100.0	.0	.0	.0		744		0	
	** PROE	LEMS/SOLUTI	ONS/COMMENTS							
				R MAJOR MODIFI IS INCLUDED RE E.						
11/81	A	27.0	.0	.0	.0					
- <b>-</b>	B	27.0	.0	.0	.0					
	SYSTEM	27.0	.0	.0	.0		720		0	

	MODULE	AVAÎLABILÎ	TY OPERABILITY	RELIABILITY	UTILIZATION	% REMOVAL SO2 PART.				CAP.
	** PROE	BLEMS/SOLUT	TIONS/COMMENTS							
			BURTUS HOUSEN	ED M4 100 M00:		THE ECD EVE	TEM 811	TUODIC I		
			DURING NOVEME ED. THIS WOR WITH GUNITE.							
			DURING THE MO	NTH ADDITION	AL OUTAGE TIM	E WAS DUE T	O GENER	RAL FGD	MAINTE	HANCE
12/81	A	88.0	83.0		66.0					
	В	88.0		93.0	66.0		<b>-</b>			
	SYSTEM	88.0	83.0	93.0	66.0		744	592	491	
	** PROE	BLEMS/SOLUT	IONS/COMMENTS							
			DURING DECEMB	ER MISCELLAN	EOUS EQUIPMEN	T PROBLEMS	WERE EN	COUNTER	RED.	
			ALSO DURING T	HE MONTH OPAC	CITY MONITORS	WERE INSTA	LLED AN	ND TESTE	ED.	
1/82	A	100.0	88.0	95.0	70.0					
	В		88.0	95.0	70.0					
	SYSTEM	100.0	88.0	95.0	70.0		744	592	521	
2/82	A	98. <b>0</b>	87.0	92.0	60.0					
	В	99.0		90.0	62.0					
	SYSTEM	98.5	88.5	94.0	61.0		672	463	410	
3/82	A	99.0	88.0	91.0	80.0					
	В	99.0	92.0	91.0 95.0	80.0 83.0					
	SYSTEM	99.0	90.0	93.0	81.5		744	673	606	
	** PROB	SLEMS/SOLUT	IONS/COMMENTS							
			THE UTILITY R			-RELATED PR	OBLEMS	WERE EN	NCOUNTE	RED
4/82	A	100.0	89.0	96.0	63.0					
4/82	A B	100.0 100.0		96.0 94.0	63.0 62.0					
4/82		100.0	88.0				720	509	450	
	B SYSTEM	100.0	88.0 88.5	94.0 95.0	62.0 62.5		720	509	450	
4/82 5/82	B SYSTEM	100.0	88.0 88.5	94.0	62.0		720	509	450	
	B SYSTEM	100.0 100.0 100.0 100.0	88.0 88.5 66.0	94.0 95.0 97.0	62.0 62.5 23.0		720 744		450 171	
5/82	B SYSTEM A B SYSTEM	100.0 100.0 100.0 100.0 100.0	88.0 88.5 66.0 66.0 66.0	94.0 95.0 97.0 97.0 97.0	62.0 62.5 23.0 23.0 23.0					
	B SYSTEM A B	100.0 100.0 100.0 100.0 100.0	88.0 88.5 66.0 66.0 66.0	94.0 95.0 97.0 97.0 97.0	62.0 62.5 23.0 23.0 23.0					
5/82	B SYSTEM A B SYSTEM	100.0 100.0 100.0 100.0 100.0	88.0 88.5 66.0 66.0 66.0	94.0 95.0 97.0 97.0 97.0	62.0 62.5 23.0 23.0 23.0			259	171	
5/82	B SYSTEM A B SYSTEM A B SYSTEM	100.0 100.0 100.0 100.0 100.0 100.0	88.0 88.5 66.0 66.0 66.0 86.0	94.0 95.0 97.0 97.0 97.0 96.0 99.0	62.0 62.5 23.0 23.0 23.0 46.0 47.0		744	259	171	
5/82	B SYSTEM A B SYSTEM A B SYSTEM	100.0 100.0 100.0 100.0 100.0 100.0	88.0 88.5 66.0 66.0 66.0 89.0 87.5	94.0 95.0 97.0 97.0 97.0 96.0 99.0 97.5	62.0 62.5 23.0 23.0 23.0 46.0 47.0 46.5	-RELATED PR	744 720	259 383	171 335	RED
5/82	B SYSTEM A B SYSTEM A B SYSTEM ** PROB	100.0 100.0 100.0 100.0 100.0 100.0	88.0 88.5 66.0 66.0 86.0 89.0 87.5 TIONS/COMMENTS	94.0 95.0 97.0 97.0 97.0 96.0 99.0 97.5	62.0 62.5 23.0 23.0 23.0 46.0 47.0 46.5 NO MAJOR FGE	P-RELATED PR	744 720	259 383	171 335	RED
5/82 6/82	B SYSTEM A B SYSTEM A B SYSTEM ** PROB	100.0 100.0 100.0 100.0 100.0 100.0 100.0 8LEMS/SOLUT	88.0 88.5 66.0 66.0 86.0 89.0 87.5 TIONS/COMMENTS THE UTILITY R	94.0 95.0 97.0 97.0 97.0 96.0 99.0 97.5	62.0 62.5 23.0 23.0 23.0 46.0 47.0 46.5	-RELATED PR	744 720	259 383	171 335	RED
5/82 6/82	B SYSTEM A B SYSTEM A B SYSTEM ** PROB	100.0 100.0 100.0 100.0 100.0 100.0 100.0 8LEMS/SOLUT	88.0 88.5 66.0 66.0 86.0 89.0 87.5 TIONS/COMMENTS THE UTILITY R DURING THE SE	94.0 95.0 97.0 97.0 97.0 96.0 99.0 97.5 EPORTED THAT	62.0 62.5 23.0 23.0 23.0 46.0 47.0 46.5 NO MAJOR FGC 1982.	-RELATED PR	744 720	259 383 WERE E	171 335 NCOUNTE	
5/82 6/82 7/82	B SYSTEM A B SYSTEM A B SYSTEM ** PROB	100.0 100.0 100.0 100.0 100.0 100.0 100.0 8LEMS/SOLUT	88.0 88.5 66.0 66.0 86.0 89.0 87.5 FIONS/COMMENTS THE UTILITY R DURING THE SE 92.9 95.9 94.4	94.0 95.0 97.0 97.0 97.0 96.0 99.0 97.5 EPORTED THAT COND QUARTER 93.7 96.8 95.2	62.0 62.5 23.0 23.0 46.0 47.0 46.5 NO MAJOR FGC 1982. 62.6 64.7 63.7	P-RELATED PR	744 720 OBLEMS	259 383 WERE E	171 335 NCOUNTE	FRED 50.2
5/82 6/82	B SYSTEM A B SYSTEM A B SYSTEM ** PROB	100.0 100.0 100.0 100.0 100.0 100.0 100.0 8LEMS/SOLUT	88.0 88.5 66.0 66.0 86.0 89.0 87.5 TIONS/COMMENTS THE UTILITY R DURING THE SE 92.9 95.9	94.0 95.0 97.0 97.0 97.0 96.0 99.0 97.5 EPORTED THAT COND QUARTER 93.7 96.8	62.0 62.5 23.0 23.0 23.0 46.0 47.0 46.5 NO MAJOR FGE 1982.	P-RELATED PR	744 720 OBLEMS	259 383 WERE E	171 335 NCOUNTE	

91.3

91.9

91.6

75.3

75.8

75.6

720

600

544 64.9

9/82 6A

6B

SYSTEM

97.2

96.5

96.8

90.4

91.0

90.7

PERIOD	MODULE AVA	ILABILI	TY OPERABILITY		UTILIZATION	S02	PART.	HOURS	BOILER HOURS		
	** PROBLEM	IS/SOLUT	IONS/COMMENTS								
			THE UTILITY R			_		_	WERE E	NCOUNT	ERED
10/00		77 7	<b>50</b> 6	300.0	24.7						
10/82	6A 6B	33.3	93.2	100.0 94.6	24.7						
	SYSTEM	33.2	95.8	97.3	24.1			744	187	179	17.8
	** PROBLEM	IS/SOLUT	IONS/COMMENTS								
			UNIT 6 WAS OU	T OF SERVICE	DURING PART	OF OC	TOBER (	FOR AN	ANNUAL	OUTAG	Ε.
11/82	4.4	46 7	81.5	78.3	75 7						
11/02	6B	46.5	76 1	70.3	35./ 77.7						
	SYSTEM	46.4	78.8	73.0 75.6	34.5			720	315	248	31.9
			IONS/COMMENTS		52			,			
	AA TROBELL	157 50 201	UNIT 6 WAS OU		DURING PART	OF NO	VEMBER	FOR T	HE ANNU.	AL OUT	AGE.
						0, 1,0		. •			
12/82		98.0		88.0							
	6B	96.9	87.1	87.2	63.9						
	SYSTEM	97.5	87.5	87.6	64.2			744	546	478	58.3
1/83	6 <b>A</b>	96.7	88.5 88.4	90.6	55.6						
	6B	96.8	88.4	90.5	55.6						
	SYSTEM	96.7	88.4	90.5	55.6			744	468	414	45.1
	** PROBLEM	1 <b>5</b> /50LUT	IONS/COMMENTS								
			THE UTILITY FOURING DECEME					OBLEMS	WERE E	нсоинті	ERED
2/83	6A	90.9	82.4	85.2	61.5						
	6B	91.4	84.1	87.0	62.8						
	SYSTEM	91.2	83.3	87.0 86.1	62.1			672	501	418	45.0
	** PROBLEM	1S/SOLUT	IONS/COMMENTS								
			PRIOR TO FEBRAVAILABLE TINDURING A UNITOF AVAILABILE PERIODS.	TE TO INCLUDE FOUTAGE. TH	PERIODS WHEN	4 SCRU 4 CONF	BBER M ORMS T	AINTEN O THE	ANCE WA CORRECT	S PERF	
3/83	6A	88.8	86.6	87.5	80.2						
	6B	90.2	89.6	90.5	82.9						
	SYSTEM	89.5	88.1	89.0	81.6			744	689	607	61.7
	** PROBLEM	1 <b>5</b> /50LUT	IONS/COMMENTS								
			THE UTILITY F		NO MAJOR FGI	D-RELA	TED PR	OBLEMS	WERE E	NCOUNT	ERED
4/83	6A	80.4	79.6	80.3	79.6						
	6B	96.3	95.4	96.2	95.4						
	SYSTEM	88.3	87.5	88.2	87.5			720	720	630	67.1

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY ATTRIBUTED THE VERY GOOD PERFORMANCE OF MODULE 6B DURING APRIL TO PROPER MAINTENANCE PERFORMED AND THE COMPLETION OF ESSENTIAL CHANGES IN THE SCRUBBING SYSTEM DESIGN.

5/83	6A	94.5	80.0	82.4	22.6				
	6B	96.0	85.2	87.7	24.1				
	SYSTEM	95.2	82.6	85.0	23.3	744	210	174	17.7

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT OUTAGE TIME WAS ATTRIBUTED TO THE CLEANING OF MIST ELIMINATORS DURING MAY.

MAINTENANCE WORK ON MIST ELIMINATOR PUMPS ALSO CAUSED OUTAGE TIME IN MAY.

A 72 HOUR OUTAGE OCCURRED DUE TO A CHEMICAL IMBALANCE OF THE MAKEUP WATER POND. DRAINAGE FROM THE CLEANING OF AN AIR HEATER PRODUCED ACIDIC CONDITIONS IN THE POND.

6/83	6A	95.0	84.0	89.2	28.8				
	6B	96.8	86.9	92.2	29.7				
	SYSTEM	95.9	85.4	90.7	29.2	720	246	211	24.1

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING JUNE.

7/83	6A 6B SYSTEM	94.9 95.6 95.2	86.8 88.3 87.5	88.9 9 <b>0.</b> 4 89. <b>6</b>	39.8 40.5 40.1	744	341	299	32.0
8/83	6A 6B System	87.0 91.1 89.0	92.4 95.1 93.8	93.5 96.2 94.9	73.7 75.8 74.7	744	593	<b>5</b> 56	47.0
9/83	6A 6B SYSTEM	93.3 93.2 93.3	91.3 90.8 91.0	92.0 91.5 91.8	49.6 49.3 49.4	720	391	356	<b>33.</b> 3

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE PERIOD OF JULY THROUGH SEPTEMBER, 1983.

10/83	6 A	98.9	98.9	98.9	61.7				
	6B	99.6	99.8	99.8	62.2				
	SYSTEM	99.3	99.4	99.4	62.0	744	464	461	44.4

### ** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURING OCTOBER.

11/83	6A	76.7	96.1	96.1	51.4			
	6B	<b>76.1</b>	95.1	95.1	50.8			
	SYSTEM	76.4	95.6	95. <b>6</b>	51.1	720	385	368 33.7

744

334

243 26.1

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT ANNUAL OUTAGES OCCURRED DURING NOVEMBER FOR UNITS 5 AND 6.

12/83	A	38.6	69.8	75.4	31.3
	В	41.3	75.7	81.9	34.0
	SYSTEM	39.9	72.8	78.6	32.7

### ** PROBLEMS/SOLUTIONS/COMMENTS

LOSS OF LINE FEED DUE TO FROZEN WATER LINES ON THE SLAKERS CONTRIBUTED TO FGD SYSTEM DOWN TIME DURING DECEMBER.

A MODULE OUTAGE WAS REQUIRED TO CLEAN PLUGGED ABSORBER & MIST ELIMINATOR SPRAY NOZZLES.

THE UNAVAILABILITY OF THE SLUDGE TREATMENT FACILITY DURING DECEMBER CONTRIBUTED TO FGD SYSTEM DOWN TIME.

1/84	A	96.2	93.9	95.2	73.9				
	В	96.8	94.5	95.8	74.5				
	SYSTEM	96.5	94.2	95.5	74.2	744	586	552	54.0

#### ** PROBLEMS/SOLUTIONS/COMMENTS

PLUGGED RECYCLE, MIST ELIMINATOR AND PRESATURATOR SPRAY NOZZLES CONTRIBUTED TO DOWN TIME IN JANUARY.

DAMPER OPERATION FAILURE OCCURRED DURING THE MONTH.

COMPUTER-RELATED PROBLEMS WERE ENCOUNTERED DURING JANUARY.

2/84	6 <b>A</b>	95.8	73.8	84.9	23.4				
	6B	79. <b>3</b>	81.0	93.2	25.7				
	SYSTEM	87 <b>.6</b>	77.4	89.1	24.6	696	221	171	18.6

### ** PROBLEMS/SOLUTIONS/COMMENTS

PROBLEMS WITH PLUGGED SPRAY NOZZLES WERE REPORTED IN THE MIST ELIMINATOR, RECYCLE SYSTEM AND PRESATURATOR.

A POWER FAILURE AT THE SLUDGE TREATMENT PLANT OCCURRED DURING THE MONTH.

ABSORBER LINER FAILURE WAS REPORTED DURING FEBRUARY.

3/84	A	99.9	98.1	100.0	57.0			
	В	75.4	93.1	94.8	54.0			
	SYSTEM	87.6	95.6	97.4	55.5	744	432	413 40.7

### ** PROBLEMS/SOLUTIONS/COMMENTS

PRESATURATOR PLUGGAGE ACCOUNTED FOR 8 HOURS OF OUTAGE TIME IN MARCH.

COMPUTER-RELATED PROBLEMS WERE REPORTED DURING MARCH.

ABSORBER LINER FAILURE RESULTED IN 5 HRS. OF DOWN TIME IN MARCH.

THE UTILITY REPORTED THAT MODULE B WAS UNAVAILABLE 160 HOURS DUE TO DAMPER FAILURE.

4/84 6A 100.0 99.8 100.0 59.0

COLUMBUS & SOUTHERN OHIO ELEC: CONESVILLE 6 (CONT.)

				PERFORMA	NCE DATA	 			
PERIOD	MODULE	AVAILABILITY					BOILER HOURS		CAP. FACTOR
*****	6B SYSTEM	100.0 100.0	99.8 99.8	100.0 100.0	59.0 59.0	720	426	425	40.5
5/84	6A 6B SYSTEM	100.0 99.9 99.9	99.0 99.0 99.0	100.0 100.0 100.0	41.9 41.9 41.9	744	315	312	32.0
6/84	6A 6B SYSTEM	100.0 100.0 100.0	97.6 97.6 97.6	100.0 100.0 100.0	60.6 60.6 60.6	720	447	436	44.5
7/84	6A 6B SYSTEM	99.7 99.7 99.7	97.1 97.1 97.1	99.4 99.4 99.4	57.2 57.2 57.2	744	438	426	

^{**} PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD RELATED PROBLEMS WERE ENCOUNTERED DURING THE PERIOD OF APRIL THROUGH JULY, 1984.

8/84	SYSTEM	744
9/84	SYSTEM	720

^{**} PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR AUGUST AND SEPTEMBER 1984.

## SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COMPANY NAME		POWER ASSOCIATION	
PLANT NAME	COAL CREEK		
UNIT NUMBER	1		
CITY	UNDERWOOD		
STATE	NORTH DAKOT	Δ,	
REGULATORY CLASSIFICATION	D		
PARTICULATE EMISSION LIMITATION - NG/J	43.	( .100 LB/MMBTU)	
SO2 EMISSION LIMITATION - NG/J	516.	( 1.200 LB/MMBTU)	
NOX EMISSION LIMITATION - NG/J	*****	( 1.200 LB/MMBTU) (***** LB/MMBTU)	
NET PLANT GENERATING CAPACITY - MW	1100		
GROSS UNIT GENERATING CAPACITY - MW	550		
NET UNIT GENERATING CAPACITY W/FGD - MW	500		
NET UNIT GENERATING CAPACITY WO/FGD - MW	501		
EQUIVALENT SCRUBBED CAPACITY - MW	327		
** UNIT DATA - BOILER AND STACK			
BOILER SUPPLIER	COMBUSTION		
BOILER TYPE	PULVERIZED (	COAL	
BOILER SERVICE LOAD	BASE		
DESIGN BOILER FLUE GAS FLOW - CU.M/S	1038.18	(2200000 ACFM)	
BOILER FLUE GAS TEMPERATURE - C	160.0	( 320 F) ( 658 FT)	
STACK HEIGHT - M	201.	( 658 FT)	
STACK SHELL	CONCRETE		
STACK TOP DIAMETER - M	6.7	( 22.0 FT)	
** FUEL DATA			
FUEL TYPE	COAL		
FUEL GRADE	COAL		
, , , , , , , , , , , , , , , , , , , ,	LIGNITE	( (050 PTI/ID)	
AVERAGE HEAT CONTENT - J/G RANGE HEAT CONTENT - BTU/LB	14330.	( 6258 BTU/LB)	
AVERACE ACH CONTENT - BIU/LB	7.16	3068-7660	
AVERAGE ASH CONTENT - X	7.14		
RANGE ASH CONTENT - 2	3.9-16.0		
AVERAGE MOISTURE CONTENT - %	39.83 27.8-52 <i>.</i> 6		
RANGE MOISTURE CONTENT - %  AVERAGE SULFUR CONTENT - %  RANGE SULFUR CONTENT - %  AVERAGE SULFUR CONTENT - %			
AVERAGE SULFUR CUNTENT - Z	.63		
RANGE SULFUR CONTENT - 2	0.2-1.4		
AVERAGE CHLORIDE CONTENT - %	.02		
RANGE CHLORIDE CONTENT - %	0.00-0.08		
*** PARTICLE CONTROL			
** MECHANICAL COLLECTOR			
NUMBER	0		
TYPE	HONE		
** ESP			
NUMBER	1		
NUMBER OF SPARES	ō		
TYPE	COLD SIDE		
SUPPLIER	WHEELABRATO	D-FDYF	
INLET FLUE GAS CAPACITY - CU.M/S	1090.1	(2310000 ACFM)	
INLET FLUE GAS TEMPERATURE - C	160.6	( 321 F)	
PRESSURE DROP - KPA	.6	( 3. IN-H20)	
PARTICLE REMOVAL EFFICENCY - %	99.5	( 3. 11-1120)	
FARTICLE REHOVAL EFFICENCY - 7.	77.3		
** PARTICLE SCRUBBER			
NUMBER	0		
GENERIC TYPE	NONE		
SPECIFIC TYPE	N/A		
TRADE NAME/COMMON NAME	N/A		
GAS CONTACTING DEVICE TYPE	N/A		
*** FGD SYSTEM			
** GENERAL DATA			
SALEABLE PRODUCT/THROWAWAY PRODUCT	THROWAWAY P	RODUCT	
SO2 REMOVAL MODE	WET SCRUBBI		
PROCESS TYPE	LIME/ALKALI		
PROCESS ADDITIVES	NONE		

```
COMBUSTION ENGINEERING
    SYSTEM SUPPLIER
                                                       BLACK & VEATCH
    A-E FIRM
                                                       FULL SCALE
    DEVELOPMENT LEVEL
    NEW/RETROFIT
                                                      NEW
    UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.50
    UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                          54.00
    ENERGY CONSUMPTION - %
                                                            . 2
    CURRENT STATUS
                                                        1
    COMMERCIAL START-UP
                                                        8/79
    INITIAL START-UP
                                                        7/79
    CONTRACT AWARDED
                                                        5/76
** DESIGN AND OPERATING PARAMETERS
                                                     8091.6 ( 87100 SQ FT)
    SPACE REQUIREMENTS - SQ M
                                                       72.0
    OPER. & MAINT. REQUIREMENT - MANHR/DAY
** QUENCHER/PRESATURATOR
    NUMBER
                                                        0
** ABSORBER
   NUMBER
                                                        4
    NUMBER OF SPARES
                                                       0
    GENERIC TYPE
                                                      SPRAY TOWER
    SPECIFIC TYPE
                                                      OPEN COUNTERCURRENT SPRAY
    TRADE NAME/COMMON TYPE
                                                      N/A
    SUPPLIER
                                                      COMBUSTION ENGINEERING
    DIMENSIONS - FT
                                                      21.5 WIDE X 20 DEEP X 55 HIGH
    SHELL GENERIC MATERIAL
                                                      STAINLESS STEEL
    SHELL SPECIFIC MATERIAL
                                                      AUSTENITIC
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                                      TYPE 316L
    LINER GENERIC MATERIAL
                                                      NONE
    LINER SPECIFIC MATERIAL
                                                      N/A
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                                      N/A
    GAS CONTACTING DEVICE TYPE
                                                      NONE
    NUMBER- OF CONTACTING ZONES
                                                     1
    NUMBER- OF CONTACTING ZONES

LIQUID RECIRCULATION RATE - LITER/S

L/G RATIO - L/CU.M

GAS-SIDE PRESSURE DROP - KPA

SUPERFICAL GAS VELOCITY - M/SEC

INLET GAS FLOW - CU. M/S

INLET GAS TEMPERATURE - C

100.6 FT/S

110.0 (20790 GPM)

(60.0 GAL/1000 ACF)

110.6 FT/S

(10.6 FT/S)

(10.6 FT/S)
    SO2 REMOVAL EFFICIENCY - X
                                                          90.0
** MIST ELIMINATOR
    PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                                     PRIMARY COLLECTOR
    NUMBER PER SYSTEM
                                                        4
    NUMBER OF SPARES PER SYSTEM
                                                       0
    NUMBER PER MODULE
                                                       1
    GENERIC TYPE
                                                     IMPINGEMENT
    SPECIFIC TYPE
                                                      BAFFLE
    TRADE NAME/COMMON TYPE
                                                      CLOSED VANE
    CONFIGURATION
                                                     HORIZONTAL
    NUMBER OF STAGES
                                                    2
2.44
76.20
7.6
.1
                                                        2
    NUMBER OF PASSES PER STAGE
    FREEBOARD DISTANCE - M
                                                                      ( 8.0 FT)
(30.0 IN)
( 3.00 IN)
    DISTANCE BETHEEN STAGES - CM
    DISTANCE BETHEEN VANES - CM
    PRESSURE DROP - KPA
                                                                      ( .5 IN-H20)
( 8.9 FT/S)
    CONSTRUCTION MATERIAL GENERIC TYPE ORGANIC
CONSTRUCTION MATERIAL SPECIFIC TYPE FIBER-RET
WASH WATER SOURCE
                                                     FIBER-REINFORCED POLYESTER
                                                      COOLING TOWER BLOWDOWN
    WASH FREQUENCY
                                                      INTERMITTENT
    WASH RATE - L/S
                                                          37.8
                                                                    ( 600 GAL/MIN)
** REHEATER
   NUMBER
                                                       1
    NUMBER OF SPARES
                                                        0
    GENERIC TYPE
                                                      RYPASS
    SPECIFIC TYPE
                                                      COLD SIDE
    TRADE NAME/COMMON TYPE
                                                      N/A
```

PERCENT GAS BYPASSED - AVG 40.0 TEMPERATURE INCREASE - C 47.2 85 F) ( 135 F) INLET FLUE GAS TEMPERATURE - C 57.2 OUTLET FLUE GAS TEMPERATURE - C 98.9 ( 210 F) CONSTRUCTION MATERIAL GENERIC TYPE ND CONSTRUCTION MATERIAL SPECIFIC TYPE NR ** FANS NUMBER 4 NUMBER OF SPARES 0 CENTRIFUGAL DESIGN SUPPLIER GREEN FAN FUNCTION BALANCED DRAFT FORCED DRAFT APPLICATION SERVICE DRY FLUE GAS FLOW RATE - CU.M/S 163.51 ( 346500 ACFM) FLUE GAS TEMPERATURE - C 160.6 ( 321 F) PRESSURE DROP - KPA 12.8 (42.0 IN-H20) CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL ** DAMPERS NUMBER FUNCTION **ISOLATION** GENERIC TYPE LOUVER SPECIFIC TYPE NΒ CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL CONSTRUCTION MATERIAL SPECIFIC TYPE HIGH STRENGTH LOW ALLOY [HSLA] LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DAMPERS NUMBER FUNCTION ISOLATION GENERIC TYPE LOUVER SPECIFIC TYPE NR CONSTRUCTION MATERIAL GENERIC TYPE STAINLESS STEEL CONSTRUCTION MATERIAL SPECIFIC TYPE AUSTENITIC LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DAMPERS NUMBER **FUNCTION** CONTROL GENERIC TYPE LOUVER SPECIFIC TYPE NR CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL CONSTRUCTION MATERIAL SPECIFIC TYPE HIGH STRENGTH LOW ALLOY [HSLA] LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DAMPERS NUMBER FUNCTION ISOLATION GENERIC TYPE LOUVER ΝR SPECIFIC TYPE CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL CONSTRUCTION MATERIAL SPECIFIC TYPE HIGH STRENGTH LOW ALLOY [HSLA] LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DUCTWORK OUTLET LOCATION STAINLESS STEEL SHELL GENERIC MATERIAL TYPE AUSTENITIC SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DUCTHORK LOCATION INLET SHELL GENERIC MATERIAL TYPE CARBON STEEL SHELL SPECIFIC MATERIAL TYPE AISI 1110

COOPERATIVE POWER ASSOCIATION: COAL CREEK 1 (CONT.)

LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE N/A

** DUCTWORK

BYPASS LOCATION CARBON STEEL SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE AISI 1110 LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A

** DUCTWORK

PLENUM TO STACK LOCATION SHELL GENERIC MATERIAL TYPE CARBON STEEL SHELL SPECIFIC MATERIAL TYPE AISI 1110 LINER GENERIC MATERIAL TYPE INORGANIC

HYDRAULICALLY-BONDED MORTAR LINER SPECIFIC MATERIAL TYPE

** REAGENT PREPARATION EQUIPMENT

FUNCTION SLAKER DEVICE NR DEVICE TYPE NR MANUFACTURER WALLACE & TIERMAN NUMBER 2 PRODUCT QUALITY - % SOLIDS 10.0

** TANKS

SERVICE NUMBER ----------ABSORBER RECYCLE 2 FLYASH *** REAGENT PREP PRODUCT ***

** PUMPS

SERVICE NUMBER _____ BLEED STREAM ٦ SLURRY FEED 2 REACTION TANK TRANSFER 6

** SOLIDS CONCENTRATING/DEWATERING

DEVICE NONE

*** SLUDGE

** TREATMENT

METHOD NONE DEVICE NR PROPRIETARY PROCESS N/A

** DISFOSAL NATURE

FINAL TYPE POND LOCATION ON-SITE SITE TRANSPORTATION METHOD PIPELINE SITE TREATMENT CLAY LINING SITE DIMENSIONS 400 ACRES SITE SERVICE LIFE - YRS 35

** PROCESS CONTROL AND INSTRUMENTATION

CHEMICAL PARAMETERS PH, SO2 PHYSICAL VARIABLES SOLIDS, LIQUID LEVEL MONITOR TYPE UNILOC FOR PH, LEAR-SIEGLER FOR SO2, MOORE FOR S

MONITOR LOCATION REACTION TANK FOR PH

** WATER BALANCE WATER LOOP TYPE OPEN

** CHEMICALS AND CONSUMPTION

FUNCTION ABSORBENT
NAME LIME
PRINCIPAL CONSTITUENT CAO
SOURCE/SUPPLIER PETE LIEN

SOURCE/SUPPLIER PETE LIEN & SONS, INC.
CONSUMPTION RAPID CITY, SOUTH DAKOTA
POINT OF ADDITION SLAKER

** FGD SPARE CAPACITY INDICES

ABSORBER - %

** FGD SPARE COMPONENT INDICES

ABSORBER .O

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

.0

7/79 SYSTEM 744

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER BEGAN OPERATIONS IN MAY 1979. WET TEST RUNS WERE MADE WITH THE SCRUBBERS DURING THE SECOND WEEK OF JULY AND THE SYSTEM WAS OPERATED WITH LIME SLURRY DURING THE THIRD WEEK OF JULY. THE UTILITY BEGAN INITIAL FGD SYSTEM OPERATIONS AS DEFINED BY THE UTILITY (24-HOUR MINIUM PERIOD) ON JULY 19.

8/79 SYSTEM 744

9/79 SYSTEM 720

### ** PROBLEMS/SOLUTIONS/COMMENTS

THIS UNIT STARTED COMMERCIAL OPERATIONS ON AUGUST 1, 1979. SOME MINOR SHAKEDOWN PROBLEMS WERE REPORTED FOR THE AUGUST-SEPTEMBER PERIOD.

 10/79
 SYSTEM
 744
 711

 11/79
 SYSTEM
 720
 703

 12/79
 SYSTEM
 744
 719

### ** PROBLEMS/SOLUTIONS/COMMENTS

SINCE STARTUP THE UNIT HAS EXPERIENCED NUMEROUS SHAKEDOWN PROBLEMS BOTH BOILER AND FGD SYSTEM-RELATED. AFTER THE NEXT SCHEDULED OUTAGE IN APRIL, THE UTILITY EXPECTS STABLE FGD OPERATIONS TO BE ESTABLISHED.

DURING DECEMBER TWO OF THE EIGHT COAL PULVERIZERS WERE OUT OF SERVICE DUE TO A PRIMARY AIR DUCT EXPLOSION. LITTLE DOWN TIME RESULTED, HOWEVER, THE UNIT HAD TO OPERATE AT A REDUCED LOAD. NO FGD SYSTEM PROBLEMS WERE REPORTED.

1/80 SYSTEM 100.**0** 96.1 744 715 715

### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING JANUARY TWO MODULES AT A TIME WERE TAKEN OFF-LINE FOR INSPECTION AND CLEANING. SOME CRACKED NOZZLES AND PLUGGING PROBLEMS WERE FOUND DURING THE INSPECTION. THE BOILER WAS OPERATED AT A REDUCED LOAD.

SOME OUTAGE TIME DURING THE MONTH WAS CAUSED BY BOILER-RELATED PROBLEMS. A BOILER TRIP WAS CAUSED BY A TURBINE ELECTRICIAL RELAY ON JANUARY 13.

AN HOUR OF OUTAGE TIME RESULTED FROM A LOSS OF POWER TO THE CONTROL SYSTEM AND AN ABNORMAL BOILER DRUM LEVEL WAS ALSO ENCOUNTERED ON JANUARY

COOPERATIVE POWER ASSOCIATION: COAL CREEK 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

SUZ PART. NOURS NOURS FACIUR

16

A THREE TO FOUR HOUR OUTAGE WAS SCHEDULED ON JANUARY 27 TO MAKE REPAIRS ON FGD SYSTEM EQUIPMENT.

2/80 SYSTEM 99.9 696 695

### ** PROBLEMS/SOLUTIONS/COMMENTS

WHILE THE BOILER WAS OUT OF SERVICE DUE TO ID FAN PROBLEMS CAUSED BY ELECTRICAL GROUNDING, TWO MODULES WERE TAKEN OUT OF SERVICE SO CALIBRATIONS COULD BE DONE.

3/80 SYSTEM 100.0 96.1 744 715 715

### ** PROBLEMS/SOLUTIONS/COMMENTS

BOILER TRIPS OCCURRED THREE TIMES DURING THE MONTH. ONE TRIP WAS DUE TO THE CUT DOWN OF TRANSMISSION POWER ON MARCH 12.

THE FGD SYSTEM WAS SHUTDOWN WITH THE BOILER FOR FOUR HOURS TO CLEAN THE FILTER ON THE BOILER STATOR COOLING PUMPS.

DURING MARCH STACK EMISSION TESTS WERE UNDERTAKEN. THE SYSTEM OPERATED WITH ONE MODULE DOWN DURING TESTING.

4/80	11	96.7	58.3	100.0	21.4
	12	100.0	81.7	100.0	30.0
	13	100. <b>0</b>	96.1	100.0	35.3
	14	100.0	96.9	100.0	35.6
	SYSTEM	99.2	83.3	100.0	30.6

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER WAS OFF LINE FOR APPROXIMATELY 19 DAYS FOR THE ANNUAL UNIT OUTAGE. THE SCRUBBING SYSTEM WAS AVAILABLE DURING THE BOILER OUTAGE.

720

264

220 26.2

5/80	11	88.3	68.8	100.0	34.4
	12	79.3	18.6	100.0	9.3
	13	91.9	79.6	100.0	39.8
	14	91.3	35.5	100.0	17.7
	SYSTEM	87.7	50.6	100.0	25.3

STEM 87.7 50.6 100.0 25.3 744 372 188 28.2

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE ANNUAL UNIT OUTAGE WAS COMPLETED IN THE BEGINNING OF THE MONTH. THERE WERE PROBLEMS WITH BOILER STARTUP AFTER THIS OUTAGE CAUSING LOW OPERABILITY OF THE FGD SYSTEM.

6/80	11	92.9	49.3	100.0	49.2
	12	98.5	47.6	100.0	47.5
	13	74.7	42.2	100.0	42.1
	14	93.5	73.0	100.0	72.8
	SYSTEM	89.9	53.0	100.0	52.9

STEM 89.9 53.0 100.0 52.9 720 718 381 58.5

### ** PROBLEMS/SOLUTIONS/COMMENTS

THERE WERE NO MAJOR PROBLEMS REPORTED DURING JUNE. ROUTINE MAINTENANCE AND REPAIRS WERE DONE THROUGHOUT THE MONTH.

7/80 SYSTEM 100.0 100.0 100.0 87.1 744 648 648 47.1

ERIOD	MODULE AVAILABIL	ITY OPERABILITY RELIABILITY		% REMO	DVAL	PER	BOILER HOURS		CAP. FACTOR
	** PROBLEMS/SOLU	ITTONE /COMMENTS							
	** PROBLEMS/SULC	IN JULY, NO PROBLEMS WERE	ENCOLNITEDED		15 FCD	ever	. ш		
			ENCOUNTERED	MILL IL	ie rou	31311	11.		
3/80		24.8	17.5						
	12	43.5	30.6						
	13 14	42.7 78.9	30.1 55.6						
	SYSTEM	47.5	33.5			744	525	249	31.8
	** PROBLEMS/SOLU	JTIONS/COMMENTS							
		THE UTILITY REPORTED THAT	NO MAJOR FGO	-RELATE	D PRO	BLEMS	WERE EN	NCOUNT E	ERED
9/80	SYSTEM	.0	.0			720	0	0	.0
	** PROBLEMS/SOLU	JTIONS/COMMENTS							
		THE UNIT DID NOT OPERATE	DURING SEPTEM	1BER DU	E TO A	TURB	NE BEAR	RING FA	AILURE.
0/80	11	<b>65.</b> 6	13.2						
	12	80.3	16.1						
	13	2.7	.0						
	14	36.1	7.3						
	SY <b>S</b> TEM	46.2	9.3			744	149	69	12.1
	** PROBLEMS/SOLU	JTIONS/COMMENTS							
	** PROBLEMS/SOLU	JTIONS/COMMENTS  DURING MOST OF OCTOBER TH PERFORMED ON THE TURBINE HOURS DURING THE MONTH.							
1/80		DURING MOST OF OCTOBER TH PERFORMED ON THE TURBINE							
L/80		DURING MOST OF OCTOBER TH PERFORMED ON THE TURBINE HOURS DURING THE MONTH.	BEARINGS. TH						
L/8 <b>0</b>	11	DURING MOST OF OCTOBER TH PERFORMED ON THE TURBINE HOURS DURING THE MONTH. 46.7	BEARINGS. TH						
L/8 <b>0</b>	11 12 13 14	DURING MOST OF OCTOBER TH PERFORMED ON THE TURBINE HOURS DURING THE MONTH. 46.7 48.1	45.8 47.2 33.1 44.2			TED AF	PROXIM	ATELY 1	150
/8 <b>0</b>	11 12 13	DURING MOST OF OCTOBER TH PERFORMED ON THE TURBINE HOURS DURING THE MONTH. 46.7 48.1 33.7	45.8 47.2 33.1					ATELY 1	
	11 12 13 14 SYSTEM	DURING MOST OF OCTOBER TH PERFORMED ON THE TURBINE HOURS DURING THE MONTH. 46.7 48.1 33.7 45.0 43.4	45.8 47.2 33.1 44.2 42.6 60.2			TED AF	PROXIM	ATELY 1	150
	11 12 13 14 SYSTEM 11	DURING MOST OF OCTOBER TH PERFORMED ON THE TURBINE HOURS DURING THE MONTH. 46.7 48.1 33.7 45.0 43.4	45.8 47.2 33.1 44.2 42.6 60.2 30.1			TED AF	PROXIM	ATELY 1	150
	11 12 13 14 SYSTEM 11 12	DURING MOST OF OCTOBER TH PERFORMED ON THE TURBINE HOURS DURING THE MONTH. 46.7 48.1 33.7 45.0 43.4 60.6 30.3 85.0	45.8 47.2 33.1 44.2 42.6 60.2 30.1 84.4			TED AF	PROXIM	ATELY 1	150
	11 12 13 14 SYSTEM 11	DURING MOST OF OCTOBER TH PERFORMED ON THE TURBINE HOURS DURING THE MONTH. 46.7 48.1 33.7 45.0 43.4	45.8 47.2 33.1 44.2 42.6 60.2 30.1			TED AF	PROXIM	307	150
1/80 2/80	11 12 13 14 SYSTEM 11 12 13	DURING MOST OF OCTOBER TH PERFORMED ON THE TURBINE HOURS DURING THE MONTH. 46.7 48.1 33.7 45.0 43.4 60.6 30.3 85.0 10.0 46.6	45.8 47.2 33.1 44.2 42.6 60.2 30.1 84.4 9.9			720	PPROXIMA 707	307	30.8
	11 12 13 14 SYSTEM 11 12 13 14 SYSTEM	DURING MOST OF OCTOBER TH PERFORMED ON THE TURBINE HOURS DURING THE MONTH. 46.7 48.1 33.7 45.0 43.4 60.6 30.3 85.0 10.0 46.6	45.8 47.2 33.1 44.2 42.6 60.2 30.1 84.4 9.9 46.2	HE UNIT	OPERA	720 744	707 739	307 344	30.8
	11 12 13 14 SYSTEM 11 12 13 14 SYSTEM ** PROBLEMS/SOLU	DURING MOST OF OCTOBER TH PERFORMED ON THE TURBINE HOURS DURING THE MONTH.  46.7 48.1 33.7 45.0 43.4 60.6 30.3 85.0 10.0 46.6 JTIONS/COMMENTS NO MAJOR PROBLEMS WERE EN	45.8 47.2 33.1 44.2 42.6 60.2 30.1 84.4 9.9 46.2	HE UNIT	OPERA	720 744	707 739	307 344	30.8
∕80	11 12 13 14 SYSTEM 11 12 13 14 SYSTEM ** PROBLEMS/SOLU	DURING MOST OF OCTOBER TH PERFORMED ON THE TURBINE HOURS DURING THE MONTH.  46.7 48.1 33.7 45.0 43.4 60.6 30.3 85.0 10.0 46.6  JTIONS/COMMENTS NO MAJOR PROBLEMS WERE EN	45.8 47.2 33.1 44.2 42.6 60.2 30.1 84.4 9.9 46.2	HE UNIT	OPERA	720 744	707 739	307 344	30.8
2/80	11 12 13 14 SYSTEM  11 12 13 14 SYSTEM  ** PROBLEMS/SOLU  11 100.0	DURING MOST OF OCTOBER TH PERFORMED ON THE TURBINE HOURS DURING THE MONTH.  46.7 48.1 33.7 45.0 43.4 60.6 30.3 85.0 10.0 46.6  JTIONS/COMMENTS NO MAJOR PROBLEMS WERE EN	### ### ##############################	HE UNIT	OPERA	720 744	707 739	307 344	30.8
:/80	11 12 13 14 SYSTEM  11 12 13 14 SYSTEM  ** PROBLEMS/SOLU  11 100.0 12 100.0 13 100.0 14	DURING MOST OF OCTOBER TH PERFORMED ON THE TURBINE HOURS DURING THE MONTH.  46.7 48.1 33.7 45.0 43.4 60.6 30.3 85.0 10.0 46.6  JTIONS/COMMENTS  NO MAJOR PROBLEMS WERE EN 45.2 46.8 38.7 44.6	### ### ##############################	HE UNIT	OPERA	720 744	707 739 DECEMBER	307 344	30.8 72.2
2/80 1/81	11 12 13 14 SYSTEM  11 12 13 14 SYSTEM  ** PROBLEMS/SOLU  11 100.0 12 100.0 13 100.0 14 100.0 SYSTEM  100.0	DURING MOST OF OCTOBER TH PERFORMED ON THE TURBINE HOURS DURING THE MONTH.  46.7 48.1 33.7 45.0 43.4 60.6 30.3 85.0 10.0 46.6  JTIONS/COMMENTS  NO MAJOR PROBLEMS WERE EN 10.0 45.2 46.8 38.7 44.6 43.8	### ### ### ### ### ### ### ### ### ##	HE UNIT	OPERA	720 744	707 739	307 344	30.8
2/80	11 12 13 14 SYSTEM  11 12 13 14 SYSTEM  ** PROBLEMS/SOLU  11 100.0 12 100.0 14 100.0 SYSTEM 100.0	DURING MOST OF OCTOBER TH PERFORMED ON THE TURBINE HOURS DURING THE MONTH.  46.7 48.1 33.7 45.0 43.4 60.6 30.3 85.0 10.0 46.6  JTIONS/COMMENTS  NO MAJOR PROBLEMS WERE EN 345.2 46.8 38.7 44.6 43.8 57.4	## ## ## ## ## ## ## ## ## ## ## ## ##	HE UNIT	OPERA	720 744	707 739 DECEMBER	307 344	30.8 72.2
//80	11 12 13 14 SYSTEM  11 12 13 14 SYSTEM  ** PROBLEMS/SOLU  11 100.0 12 100.0 14 100.0 14 100.0 15 SYSTEM  100.0 11 82.5 12 82.5	DURING MOST OF OCTOBER TH PERFORMED ON THE TURBINE HOURS DURING THE MONTH.  46.7 48.1 33.7 45.0 43.4 60.6 30.3 85.0 10.0 46.6  JTIONS/COMMENTS  NO MAJOR PROBLEMS WERE EN  45.2 46.8 38.7 44.6 43.8 57.4 79.1	## ## ## ## ## ## ## ## ## ## ## ## ##	HE UNIT	OPERA	720 744	707 739 DECEMBER	307 344	30.8 72.2
2/80 1/81	11 12 13 14 SYSTEM  11 12 13 14 SYSTEM  ** PROBLEMS/SOLU  11 100.0 12 100.0 14 100.0 SYSTEM 100.0	DURING MOST OF OCTOBER TH PERFORMED ON THE TURBINE HOURS DURING THE MONTH.  46.7 48.1 33.7 45.0 43.4 60.6 30.3 85.0 10.0 46.6  JTIONS/COMMENTS NO MAJOR PROBLEMS WERE EN  45.2 46.8 38.7 44.6 38.7 44.6 43.8 57.4 79.1 71.8	## ## ## ## ## ## ## ## ## ## ## ## ##	HE UNIT	OPERA	720 744	707 739 DECEMBER	307 344	30.8 72.2

23.9

3/81 11 47.4 50.4

					VCE DATA UTILIZATION	% RE SO2	MOVAL PART.	PER HOURS	BOILER HOURS	FGD HOURS	CAP.
	12	47.4	73.7		34.9						
	13	47.4 47.4	57.8		27.4						
	14	47.4	58.4		29.0						
	SYSTEM	47.4	60.9		28.8			744	353	215	30.7
	** PROB	SLEMS/SOLUTION	S/COMMENTS								
				RST QUARTER 1 E REACTION TA	1981 VIBRATIO ANK BLADES.	N PROI	BLEMS :	WERE EX	KPERIEN(	CED CAL	JSING
4/81		100.0	64.7	100.0	64.7						
	12	100.0 100.0	94.7	100.0	94.7						
	13	100.0	36.7	100.0	36.7						
	14 CYCTEM	100.0 100.0	87.2	100.0	87.2			700	700	<b>53.</b>	
								720	720	510	68.6
5/81	11 12	100.0	62.9 45.4	100.0	62.9						
	13	100.0 100.0	65.6 31.5	100.0 100.0	65.6 31. <b>5</b>						
	14	100.0	39.0	100.0	39.0						
	SYSTEM	100.0	39.0 49.7	100.0 100.0 100.0	49.7			744	744	370	68.3
6/81	11	100.0	51.3	100.0	47.2						
	12	100.0	76.9	100.0	70.8						
	13	100.0 100.0	76.9 15.7	100.0	14.4						
	14	100.0 100.0	10.6	100.0	9.7						
	SYSTEM	100.0	38.6	100.0	35.6			720	663	256	57.0
	** PROB	LEMS/SOLUTION DU	RING THE SEC	COND QUARTER	1981 THE UTI	LITY I	REPORT	ED THAT	NO MA.	JOR FGD	) <b>-</b>
		RE	LATED PROBLE	MS WERE ENCO	OUNTERED.						
7/81			34.3		34.1						
	12		49.9		49.7						
	13		8.9		8.9						
	14 SYSTEM		54.8		54.6			_	_		
	3131611		37.0		36.8			744	741	274	55.3
8/81			41.5		33.3						
	12 13		46.6		37.4						
	14		8.0		6.5						
	SYSTEM		84.4 45.2		67.7 36.3			700	597	270	42.0
9/81	SYSTEM		.3.2								
97 UI		1540 (00) (5750)			.0 -			720	0	0	.0
	** FKUD	LEMS/SOLUTION									
		AL	GUST. THE L	NIT WAS TAKE	EMS WERE REPO	ORTED	FOR TH	FOR AN	HS OF .	JULY AN L OUTAG	ID SE.
10/81	11		64.7		17.5						
	12		20.9		5.6						
	13		79.6		21.5						
	14 System		49.8 53.7		13.4 14.5			744	201	108	18.4
.1/81	11							/ T T	-01	100	10.7
	12		42.0 50.4		34.2						
	13		59.4 52.2		48.3						
	14		76.2		42.5						
	SYSTEM		57.4		61.9 46.7			700	E0/	,	F0 /
			21.7		70./			720	586	536	52.6

PERIOD	MODULE	AVAILABILI	TY OPERABILITY		TY UTILIZATION	502	PART.	HOURS	HOURS	HOURS	FACTOR
	** PRO	BLEMS/SOLUT	IONS/COMMENTS								
			DURING OCTOBE	R THE UNIT	WAS SHUTDOWN	UNTIL	THE 24	TH FOR	AN ANN	UAL IN	SPEC-
12/81			72.4		54.3						
	12		67.4		50.5						
	13		49.1		36.8						
	14		49.4		37.1						
	SYSTEM		59.5		44.7			744	558	332	48.8
	** PRO	BLEMS/SOLUT	IONS/COMMENTS								
					PERFORMED ON OUTAGES WERE				ING THE	FOURTH	1
1/82	11	100 0	66.1	100.0	45 Q						
1,00	12	100.0			EQ 1						
	13	100.0	58.3 73.1	100.0	72.8						
	14	100.0	92 2	100.0	91.9						
	SYSTEM	100.0	92.2 72.4	100.0	72.2			744	741	537	81.8
2/02	11	700.0	65.8	700.0		•					
2702	12	100.0 100.0	71.3	100.0							
	13	100.0		100.0	82.9						
		100.0	04.7 E0 0	100.0	50.7						
	SYSTEM	100.0	58.9 69.7	100.0	6 <b>9.</b> 7			672	672	469	76.7
								0.2	٠.٦	,	, , , , ,
3/.82	11	100.0	37.9 50.0	100.0	37.9						
	12	100.0	50.0	100.0	50.0						
	13	100.0	39.9	100.0	39.9						
	14	100.0	30.6	100.0	30.6						
	SYSTEM	100.0	39.6	100.0	39.6			744	744	295	71.5
	** PRO	BLEMS/SOLUT	IONS/COMMENTS								
			NO MAJOR PROE		RCED OUTAGES F	IERE EN	COUNTE	RED DUT	RING TH	E FIRS	г
6/00	11	700.0	17.0	100.0	14 0						
4/02		100.0	17.0	100.0	10.9						
	12	100.0	15.6 88.3	100.0	15.5						
	13										
	14	72.4		100.0	64.5			74.		700	<b>7</b> F -
	SYSTEM	ו מפ	46.4	100.0	42.7			720	718	308	75.1

		40	AKTEK OF 17	o <b>.</b> .					
4/82	11	100.0	17.0	100.0	16.9				
	12	100.0	15.6	100.0	15.5				
	13	88.0	88.3	100.0	74.0				
	14	72.4	64.7	100.0	64.5				
	SYSTEM	90.1	46.4	100.0	42.7	720	718	308	75.1
5/82	11	100.0	3.7	100.0	3.2				
	12	100.0	13.6	100.0	11.9				
	13	100.0	52.7	100.0	46.2				
	14	100.0	54.4	100.0	47.7				
	SYSTEM	100.0	31.1	100.0	27.2	744	653	203	55.9
6/82	11	74.2	40.6	100.0	37.4				
	12	69.6	22.0	100.0	20.3				
	13	73.3	.0	100.0	54.3				
	14	76.4	52.8	100.0	48.6				
	SYSTEM	73.4	43.6	100.0	40.1	720	663	289	92.1

### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE SECOND QUARTER 1982 GENERAL MAINTENANCE AND CLEANING OF THE FGD SYSTEM ACCOUNTED FOR ANY UNAVAILABLE TIME.

7/82 SYSTEM 744

	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATI	.0N %	RE1	OVAL PART.	PER HOURS	BOILER HOURS	FGD HOURS	CAP.
								***				
8/82	SYSTEM								744			
9/82	SYSTEM								720			
10/82	SYSTEM								744			
11/82	SYSTEM								720			
12/82	SYSTEM								744			
1/83	SYSTEM								744			
2/83	SYSTEM								672			
3/83	SYSTEM								744			
	** PROB	LEMS/SOLUTION	NS/COMMENTS									
		I	NFORMATION WA	S UNAVAILABL	E FOR THE	PERI	00 0	F JULY	1982	THROUGH	MARCH	1983.
4/83	SYSTEM								720			
5/83	SYSTEM								744			
6/83	SYSTEM								720			
	** PROE	LEMS/SOLUTION	NS/COMMENTS									
		I	NFORMATION WA	S UNAVAILABL	E FOR THE	PERI	0 00	F JULY	1982	THROUGH	JUNE	1983.
7/83	SYSTEM								744			
8/83	SYSTEM								744			
9/83	SYSTEM								720			
	** PROB	LEMS/SOLUTION	IS/COMMENTS									
		TI DU	E UTILITY RE URING THE THI	PORTED THAT I	NO MAJOR F 1983.	FGD-R	ELAT	ED PRO	BLEMS	WERE EN	ICOUNTE	RED
10/83	SYSTEM								744			
11/83	SYSTEM								720			
12/83	SYSTEM								744			
	** PROB	LEMS/SOLUTION	IS/COMMENTS									
		T: A\	HE UTILITY REVALLABLE THRO	PORTED THAT OUGHOUT THE F	THE FGD S	YSTEM RTER	AT OF 1	COAL ( 983.	REEK 1	WAS 10	O PERC	ENT
1/84	SYSTEM								744			
2/84	SYSTEM								696			
3/84	SYSTEM								744			
4/84	SYSTEM								720			
5/84	SYSTEM								744			
6/84	SYSTEM								720			

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

7/84 SYSTEM

744

### ** PROBLEMS/SOLUTIONS/COMMENTS

FGD SYSTEM AVAILABILITY FOR THE PERIOD OF JANUARY THROUGH JULY 1984 WAS REPORTED AS 100%.

8/84 SYSTEM

744

### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE SCHEDULED OUTAGE IN AUGUST, CORRODING REHEAT DUCTWORK WAS REPLACED WITH 316L STAINLESS STEEL.

9/84 SYSTEM

720

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED REPLACING DETERIORATING MIST ELIMINATOR FIBERGLASS LININGS DURING THE FIRST THREE QUARTERS OF 1984.

# SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COOPERATIVE POWER ASSOCIATION COMPANY NAME CAMBETU)

CAMBETUNIT GENERATING CAPACITY - MW

CAMBETUNIT GENERATING CAPACITY - MW

CAMBETUNIT GENERATING CAPACITY W/FGD - MW

CAM COAL CREEK PLANT NAME BOILER SERVICE LOAD

BASE

DESIGN BOILER FLUE GAS FLOW - CU.M/S

BOILER FLUE GAS TEMPERATURE - C

STACK HEIGHT - M

STACK SHELL

STACK TOP DIAMETER - M

6.7

CONCRETE

CONCRETE ** FUEL DATA FUEL TYPE COAL LIGNITE 14556. FUEL GRADE AVERAGE HEAT CONTENT - J/G ( 6258 BTU/LB) RANGE HEAT CONTENT - BTU/LB 7.14 3068-7660 AVERAGE ASH CONTENT - X 7.14 3.9-16.0 39.83 27.8-52.6 RANGE ASH CONTENT - % RANGE ASH CONTENT - %

AVERAGE MOISTURE CONTENT - %

RANGE MOISTURE CONTENT - %

AVERAGE SULFUR CONTENT - %

PANGE SULFUR CONTENT - % .63 RANGE SULFUR CONTENT - % 0.2-1.4 AVERAGE CHLORIDE CONTENT - % .02 RANGE CHLORIDE CONTENT - % 0.00-0.08 *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER TYPE NONE ** ESP NUMBER 1 NUMBER OF SPARES TYPE COLD SIDE SUPPLIER WHEELABRATOR-FRYE INLET FLUE GAS CAPACITY - CU.M/S

INLET FLUE GAS TEMPERATURE - C

PRESSURE DROP - KPA

PARTICLE REMOVAL EFFICENCY - Z

1090.1

(2310000 ACFM)

1090.1

(2310000 ACFM)

1090.1

(321 F)

(3. IN-H20) ** PARTICLE SCRUBBER NUMBER GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL N/A LINER GENERIC MATERIAL N/A LINER SPECIFIC MATERIAL N/A GAS CONTACTING DEVICE TYPE N/A

*** FGD SYSTEM

```
** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                              THROWAWAY PRODUCT
   SO2 REMOVAL MODE
                                              WET SCRUBBING
   PROCESS TYPE
                                              LIME/ALKALINE FLYASH
   PROCESS ADDITIVES
                                              NONE
   SYSTEM SUPPLIER
                                              COMBUSTION ENGINEERING
                                              BLACK & VEATCH
   A-E FIRM
   DEVELOPMENT LEVEL
                                              FULL SCALE
   NEW/RETROFIT
                                              NEW
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.50
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                 54.00
   ENERGY CONSUMPTION - %
                                                  .2
   CURRENT STATUS
   COMMERCIAL START-UP
                                               9/80
   INITIAL START-UP
                                               7/80
   CONTRACT AWARDED
                                               5/76
** DESIGN AND OPERATING PARAMETERS
   SPACE REQUIREMENTS - SQ M
                                               8091.6
                                                           ( 87100 SQ FT)
   OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                72.0
** QUENCHER/PRESATURATOR
   NUMBER
                                               0
** ABSORBER
   NUMBER
                                               4
   NUMBER OF SPARES
                                               0
                                              SPRAY TOWER
   GENERIC TYPE
   SPECIFIC TYPE
                                              OPEN COUNTERCURRENT SPRAY
   TRADE NAME/COMMON TYPE
                                              N/A
                                              COMBUSTION ENGINEERING
   SUPPLIER
   DIMENSIONS - FT
                                              21.5 WIDE X 20 DEEP X 55 HIGH
    SHELL GENERIC MATERIAL
                                              STAINLESS STEEL
   SHELL SPECIFIC MATERIAL
                                              AUSTENITIC
   SHELL MATERIAL TRADE NAME/COMMON TYPE
                                              TYPE 316L
   LINER GENERIC MATERIAL
                                              NONE
   LINER SPECIFIC MATERIAL
                                              N/A
   LINER MATERIAL TRADE NAME/COMMON TYPE
                                              N/A
   GAS CONTACTING DEVICE TYPE
                                              NONE
   NUMBER OF CONTACTING ZONES
                                               1
   LIQUID RECIRCULATION RATE - LITER/S
                                               1310.
                                                             (20790 GPM)
                                               8.0
                                                             ( 60.0 GAL/1000 ACF)
   L/G RATIO - L/CU.M
                                                  .7
   GAS-SIDE PRESSURE DROP - KPA
                                                            ( 3.0 IN-H20)
                                                 3.2
   SUPERFICAL GAS VELOCITY - M/SEC
                                                            ( 10.6 FT/S)
    INLET GAS FLOW - CU. M/S
                                                163.51
                                                             ( 346500 ACFM)
                                                             ( 321 F)
    INLET GAS TEMPERATURE - C
                                                160.6
   SO2 REMOVAL EFFICIENCY - %
                                                 90.0
** MIST ELIMINATOR
                                              PRIMARY COLLECTOR
   PRE-MIST ELIMINATOR/MIST ELIMINATOR
   NUMBER PER SYSTEM
                                              4
   NUMBER OF SPARES PER SYSTEM
                                               0
   NUMBER PER MODULE
                                               1
                                              IMPINGEMENT
   GENERIC TYPE
   SPECIFIC TYPE
                                              BAFFLE
                                              CLOSED VANE
   TRADE NAME/COMMON TYPE
                                              HORIZONTAL
   CONFIGURATION
   NUMBER OF STAGES
                                                  2
   NUMBER OF PASSES PER STAGE
                                                  2
   FREEBOARD DISTANCE M
                                                 2.44
                                                            ( 8.0 FT)
   DISTANCE BETWEEN STAGES - CM
                                                 76.20
                                                             (30.0 IN)
                                                             ( 3.00 IN)
   DISTANCE BETWEEN VANES - CM
                                                  7.6
                                                             ( .5 IN-H20)
   PRESSURE DROP - KPA
                                                   .1
                                                  2.7
                                                            ( 8.9 FT/S)
   SUPERFICAL GAS VELOCITY - M/S
                                             ORGANIC
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              FIBER-REINFORCED POLYESTER
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              COOLING TOWER BLOWDOWN
   WASH WATER SOURCE
   WASH FREQUENCY
                                              INTERMITTENT
   WASH RATE L/S
                                                 37.8
                                                             ( 600 GAL/MIN)
```

** REHEATER NUMBER OF SPARES GENERIC TYPE SPECIFIC TYPE TRADE NAME/COMMON TYPE PERCENT GAS BYPASSED - AVG TEMPERATURE INCREASE - C INLET FLUE GAS TEMPERATURE - C OUTLET FLUE GAS TEMPERATURE - C CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE	1 0 BYPASS COLD SIDE N/A 40.0 47.2 ( 85 F) 57.2 ( 135 F) 98.9 ( 210 F) NR NR
** FANS NUMBER DESIGN SUPPLIER FUNCTION APPLICATION SERVICE FLUE GAS FLOW RATE - CU.M/S FLUE GAS TEMPERATURE - C PRESSURE DROP - KPA CONSTRUCTION MATERIAL GENERIC TYPE	CENTRIFUGAL GREEN FAN BALANCED DRAFT FORCED DRAFT DRY 163.51 (346500 ACFM) 160.6 (321 F) 12.8 (42.0 IN-H20) CARBON STEEL
** DAMPERS NUMBER FUNCTION GENERIC TYPE SPECIFIC TYPE CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	8 ISOLATION LOUVER NR CARBON STEEL HIGH STRENGTH LOW ALLOY [HSLA] NONE N/A
** DAMPERS NUMBER FUNCTION GENERIC TYPE SPECIFIC TYPE CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	8 ISOLATION LOUVER NR STAINLESS STEEL AUSTENITIC NONE N/A
** DAMPERS  NUMBER  FUNCTION  GENERIC TYPE  SPECIFIC TYPE  CONSTRUCTION MATERIAL GENERIC TYPE  CONSTRUCTION MATERIAL SPECIFIC TYPE  LINER GENERIC MATERIAL TYPE  LINER SPECIFIC MATERIAL TYPE	4 CONTROL LOUVER NR CARBON STEEL HIGH STRENGTH LOW ALLOY [HSLA] NONE N/A
** DAMPERS  NUMBER  FUNCTION  GENERIC TYPE  CONSTRUCTION MATERIAL GENERIC TYPE  CONSTRUCTION MATERIAL SPECIFIC TYPE  LINER GENERIC MATERIAL TYPE  LINER SPECIFIC MATERIAL TYPE	8 ISOLATION LOUVER CARBON STEEL HIGH STRENGTH LOW ALLOY [HSLA] NONE N/A
** DUCTWORK LOCATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	OUTLET STAINLESS STEEL AUSTENITIC NONE N/A

### cooperative POWER ASSOCIATION: COAL CREEK 2 (CONT.)

** DUCTWORK

LOCATION INLET

SHELL GENERIC MATERIAL TYPE CARBON STEEL

SHELL SPECIFIC MATERIAL TYPE AISI 1110

LINER GENERIC MATERIAL TYPE NONE

LINER SPECIFIC MATERIAL TYPE N/A

** DUCTWORK

LOCATION BYPASS
SHELL GENERIC MATERIAL TYPE CARBON STEEL
SHELL SPECIFIC MATERIAL TYPE AISI 1110
LINER GENERIC MATERIAL TYPE NONE
LINER SPECIFIC MATERIAL TYPE N/A

** DUCTWORK

LOCATION PLENUM TO STACK
SHELL GENERIC MATERIAL TYPE CARBON STEEL
SHELL SPECIFIC MATERIAL TYPE AISI 1110
LINER GENERIC MATERIAL TYPE INORGANIC
LINER SPECIFIC MATERIAL TYPE HYDRAULICALLY-BONDED MORTAR

** REAGENT PREPARATION EQUIPMENT

FUNCTION SLAKER

DEVICE NR

DEVICE TYPE NR

MANUFACTURER WALLACE & TIERMAN

NUMBER 2

PRODUCT QUALITY - % SOLIDS 10.0

** TANKS

SERVICE NUMBER
----ABSORBER RECYCLE 2
FLYASH ****
REAGENT PREP PRODUCT ****

** PUMPS

SERVICE NUMBER
----BLEED STREAM 3
SLURRY FEED 2
REACTION TANK TRANSFER 6

** SOLIDS CONCENTRATING/DEWATERING

DEVICE

*** SLUDGE

** TREATMENT

METHOD NONE
DEVICE NR
PROPRIETARY PROCESS N/A

** DISPOSAL

NATURE FINAL
TYPE POND

LOCATION ON-SITE
SITE TRANSPORTATION METHOD PIPELINE
SITE TREATMENT CLAY LINING
SITE DIMENSIONS 400 ACRES
SITE SERVICE LIFE - YRS 35

** PROCESS CONTROL AND INSTRUMENTATION

CHEMICAL PARAMETERS PH, SO2
PHYSICAL VARIABLES SOLIDS, LIQUID LEVEL
MONITOR TYPE UNILOC FOR PH, LEARMONITOR LOCATION REACTION TANK FOR PH

UNILOC FOR PH, LEAR-SIEGLER FOR SO2, MOORE FOR S REACTION TANK FOR PH

** WATER BALANCE WATER LOOP TYPE

OPEN

** CHEMICALS AND CONSUMPTION

FUNCTION
NAME
PRINCIPAL CONSTITUENT
SOURCE/SUPPLIER
CONSUMPTION
POINT OF ADDITION

ABSORBENT LIME CAO

PETE LIEN & SONS, INC. RAPID CITY, SOUTH DAKOTA SLAKER

** FGD SPARE CAPACITY INDICES

ABSORBER - %

.0

** FGD SPARE COMPONENT INDICES

ABSORBER

.0

At	BOUKBEK				.0						
					NCE DATA UTILIZATION	% RE	MOVAL	PER	BOILER	FGD	CAP.
									HOURS		FACTOR
7,00	0.3		<b>/3</b> 0		<b>50</b> /						
7/80			61.8		52.4						
	22		18.7		15.9						
	23		25.0		21.2						
	24		52.9		44.9						
	SYSTEM		39.6		33.6			744	631	250	34.5
	** PROB	LEMS/SOLUTION	NS/COMMENTS								
			NITIAL OPERA ROBLEMS WERE		FGD SYSTEM BE	GAN I	N JULY	1980.	NO MA	JOR ST.	ART UP
8/80	21		15.5		11.8						
	22		29.7		22.6						
	23		25.4		19.4						
	24		46.3		35.2						
	SYSTEM		58.5		44.5			744	566	331	36.1
	** PROB	LEMS/SOLUTION	NS/COMMENTS								
		BI	ELT. THIS H	AS NOT RESTR	IENCING PROBL ICTED OPERATI ALL <b>A</b> VIBRATO	ON OF	THE S	YSTEM;	HOWEVE		VEYOR
9/80	21		80.2		80.0						
• •	22		56.8		56.7						
	23		49.0								
	24		76.9		48.9						
	27		/0.9		76.7						

9/80	21	80.2	80.0				
	22	56.8	56.7				
	23	49.0	48.9				
	24	76.9	76.7				
	SYSTEM	65.7	65.6 -	720	718	472	59.1
10/80	21	92.0	91.7				
	22	86.3	86.0				
	23	22.1	22.0				
	24	70.4	70.2				
	SYSTEM			744	742		70.0
11/80	21	63.1	44.2				
	22	77.0	53.9				
	23	25.0	17.5				
	24	77.8	54.4				
	SYSTEM			720	504		41.0
12/80	21	58.7	57.5				
	22	51.3	50.3				
	23	22.2	21.8				
	24	89.4	87.6				
	SYSTEM	55.4	54.3	744	730	404	65.2
	2121511	55.4	54.3	744	730	404	65.2

		PERFORMAN	NCE DATA						
PERIOD MODULE AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% REI	MOVAL	PER	BOILER	FGD	CAP.
				S02	PART.	HOURS	HOURS	HOURS	FACTOR

### ** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR PROBLEMS HAVE BEEN ENCOUNTERED FOR THE MONTHS OF SEPTEMBER THROUGH DECEMBER.

1/81	21	99.8	75.7	75.5				
	22	99.8	37.6	37.5				
	23	99.8	46.3	46.2				
	24	99.8	68.9	68.8				
	SYSTEM	99.8	57.1	57.0	744	743	424	57.2
2/81	21	99.7	72.5	72.5				
	22	99.7	37.9	37.8				
	23	99.7	32.8	32.7				
	24	99.7	82.6	82.4				
	SYSTEM	99.7	56.5	56.4	672	670	379	57.6
3/81	21	55.4	56.3	31.2				
	22	55.4	44.7	24.7				
	23	55.4	27.7	15.3				
	24	55.4	91.3	50.5				
	SYSTEM	55.4	55.1	30.5	744	412	227	39.2

### ** PROBLEMS/SOLUTIONS/COMMENTS

OURING THE FIRST QUARTER 1981 THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED.

ON MARCH 17 THE BOILER WAS TAKEN OUT OF SERVICE FOR A BOILER/TURBINE OVERHAUL, MAINTENANCE AND MODIFICATIONS. THE UNIT WILL BE OUT OF SERVICE FOR APPROXIMATELY TEN WEEKS.

4/81	21 22 23 24	100.0 100.0 100.0 100.0			.0 .0 .0				
	SYSTEM	100.0			.0	720	0	0	.0
5/81	21	100.0			.0				
	22	100.0			. 0				
	23	100.0			.0				
	24	100.0			. 0				
	SYSTEM	100.0			.0	744	0	0	.0
6/81	21	100.0	26.5	100.0	10.3				
	22	100.0	10.0	100.0	3.9				
	23	100.0	56.6	100.0	21.9				
	24	100.0	18.6	100.0	7.2				
	SYSTEM	100.0	27.9	100.0	10.8	72 <b>0</b>	27 <del>9</del>	78	50.3

### ** PROBLEMS/SOLUTIONS/COMMENTS

UNIT WAS OFF-LINE DUE TO BOILER/TURBINE WARRANTY INSPECTION DURING THE MONTHS OF APRIL, MAY, AND PART OF JUNE.

DURING THE SECOND QUARTER 1981 THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED.

22	9.5	8.3				
23	60.6	53.2				
24	23.9	21.0				
SYSTEM	41.6	36.6	744	654	272	53.3

2/81 21		MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	ANCE DATA ( UTILIZATION	% REI	MOVAL PART.	PER HOURS	BOILER HOURS	FGD HOURS	CAP. FACTOR
22	8/01											
233	0/01					· <del>-</del>						
24 38.4 30.4 30.4 34.7 744 588 256 51 975TEM 43.5 34.4 744 588 256 51 22 91.8 90.6 22 91.8 90.6 22 91.8 90.6 32.4 82.8 81.7 975TEM 60.4 59.6 720 710 429 69.   ** PROBLEMS/SOLUTIONS/COMMENTS  *** PROBLEMS/SOLUTIONS/COMMENTS  **** PROBLEMS/SOLUTIONS/COMMENTS  **** P												
SYSTEM 43.5 34.4 744 588 256 51  7/81 21 16.6 16.4 22 91.8 90.6 23 50.1 49.4 24 82.8 61.7 SYSTEM 60.4 59.6 720 710 429 69.  *** PROBLEMS/SOLUTIONS/COMMENTS  *** PROBLEMS/SOLUTIONS/COMMENTS**  *** PROBLEMS/SOLUTIONS/COMMENTS**  *** PROBLEMS/SOLUTIONS/COMMENTS**  *** PROBLEMS/SOLUTIONS/COMMENTS**  *** PROBLEMS/SOLUTIONS/COMMENTS**  *** PROBLEMS/SOLUTIONS/COMMENTS**  *** GENERAL MAINTENANCE WAS PERFORMED ON THE FGD SYSTEM DURING THE FOURTH QUARTER. NO FGD FORCED OUTAGES WERE ENCOUNTERED.**  *** PROBLEMS/SOLUTIONS/COMMENTS**  *** GENERAL MAINTENANCE WAS PERFORMED ON THE FGD SYSTEM DURING THE FOURTH QUARTER. NO FGD FORCED OUTAGES WERE ENCOUNTERED.**  *** PROBLEMS/SOLUTIONS/COMMENTS**  *** GENERAL MAINTENANCE WAS PERFORMED ON THE FGD SYSTEM DURING THE FOURTH QUARTER. NO FGD FORCED OUTAGES WERE ENCOUNTERED.**  *** PROBLEMS/SOLUTIONS/COMMENTS**  **** PROBLEMS/SOLUTIONS/COMMENTS**  **** PROBLEMS/SOLUTIONS/COMMENTS**  **** PROBLEMS/SOLUTIONS/COMMENTS**  ***** PROBLEMS/SOLUTIONS/COMMENTS**  ***** PROBLEMS/SOLUTIONS/COMMENTS**  ********  *******  ********  ******												
97-81 21 16.6 90.6 22 91.8 90.6 22 91.8 90.6 22 91.8 90.6 24 82.8 81.7 97-55 97.6 720 710 429 69.   *** PROBLEMS/SOLUTIONS/COMMENTS  **** PROBLEMS/SOLUTIONS/COMMENTS  **** PROBLEMS/SOLUTIONS/COMMENTS  **** PROBLEMS/SOLUTIONS/COMMENTS  ***** PROBLEMS/SOLUTIONS/COMMENTS  ***** PROBLEMS/SOLUTIONS/COMMENTS  ****** PROBLEMS/SOLUTIONS/COMMENTS  ***********************************				38.4		30.4						
22 91.8 90.6 23 50.1 49.4 24 82.8 61.7 SYSTEM 60.4 59.6 720 710 429 69. *** PROBLEMS/SOLUTIONS/COMMENTS  *** PROBLEMS/SOLUTIONS/COMMENTS  *** PROBLEMS/SOLUTIONS/COMMENTS  *** PROBLEMS/SOLUTIONS/COMMENTS  *** PROBLEMS/SOLUTIONS/COMMENTS  1/61 21 54.6 54.6 22 86.8 68.8 68.8 23 76.6 76.6 24 85.7 85.7 85.7 85.7 85.7 85.7 85.7 85.7		SYSTEM		43.5		34.4			744	<b>5</b> 88	256	51.0
23	9/81											
24 82.8 61.7 SYSTEM 60.4 59.6 720 710 429 69.  *** PROBLEMS/SOLUTIONS/COMHENTS  *** PROBLEMS/SOLUTIONS/COMHENTS  *** PROBLEMS/SOLUTIONS/COMMENTS  **** PROBLEMS/SOLUTIONS/COMMENTS  **** PROBLEMS/SOLUTIONS/COMMENTS  **** PROBLEMS/SOLUTIONS/COMMENTS  ***** PROBLEMS/SOLUTIONS/COMMENTS  ***** PROBLEMS/SOLUTIONS/COMMENTS  ***********************************				91.8								
SYSTEM 60.4 59.6 720 710 429 69.  *** PROBLEMS/SOLUTIONS/COMMENTS  *** PROBLEMS/SOLUTIONS/COMMENTS**  **** PROBLEMS/SOLUTIONS/COMMENTS**  **** PROBLEMS/SOLUTIONS/COMMENTS**  *****  *****  *****  *****  *****  ****		23		50.1		49.4						
** PROBLEMS/SOLUTIONS/COMMENTS  *** PROBLEMS/SOLUTIONS/COMMENTS  **** PROBLEMS/SOLUTIONS/COMMENTS  **** PROBLEMS/SOLUTIONS/COMMENTS  ***** PROBLEMS/SOLUTIONS/COMMENTS  ********** PROBLEMS OR FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST		24		82.8		81.7						
NO FGD-RELATED PROBLEMS WERE REPORTED FOR THE THREE MONTH PERIOD.  2761 21		SYSTEM		60.4		59.6			720	71 <b>0</b>	429	69.8
21		** PROB	SLEMS/SOLUTIO	NS/COMMENTS								
22 86.8 86.8 86.8 23 76.6 76.6 24 85.7 76.6 24 85.7 75.9 75.9 744 744 565 83. 75 75.9 75.9 744 744 565 83. 75 75.9 75.9 75.9 744 744 565 83. 75 75.9 75.9 75.9 744 744 565 83. 75 75.9 91.9 91.9 23 68.1 68.1 68.1 24 80.3 80.3 75 720 720 480 67. 24 80.3 75 75.9 75.9 75.9 720 720 480 67. 26  75 75 75.9 75.9 75.9 75.9 75.9 75.9 75			И	O FGD-RELATED	PROBLEMS N	IERE REPORTED	FOR TH	E THR	EE MONT	TH PERIO	. מכ	
23 76.6 76.6 24 85.7 75.9 75.9 744 744 565 83.  1/81 21 26.4 26.4 26.4 26.4 22 91.9 91.9 23 68.1 68.1 24 80.3 80.3 80.3 80.3 80.3 80.3 80.3 80.3	0/81	21		54.6		54.6						
23 76.6 76.6 24 85.7 85.7 85.7 75.9 744 744 565 83.  L/81 21 26.4 26.4 26.4 26.4 27.2 23 68.1 68.1 68.1 24 80.3 80.3 80.3 80.3 80.3 80.3 80.3 80.3		22		86 . <b>8</b>		86.8						
24 85.7 75.9 75.9 744 744 565 83.  1/81 21 26.4 26.4 22 91.9 91.9 23 68.1 68.1 24 80.3 80.3 5YSTEM 66.7 66.7 720 720 480 67.  2/81 21 77.2 77.1 22 56.2 56.1 23 70.8 70.7 24 63.5 63.2 3 70.8 70.7 24 63.5 63.2 5YSTEM 66.9 66.8 744 743 497 68.  ** PROBLEMS/SOLUTIONS/COMMENTS     GENERAL HAINTENANCE WAS PERFORMED ON THE FGD SYSTEM DURING THE FOURTH QUARTER. NO FGD FORCED OUTAGES WERE ENCOUNTERED.    SENERAL HAINTENANCE WAS PERFORMED ON THE FGD SYSTEM DURING THE FOURTH QUARTER. NO FGD FORCED OUTAGES WERE ENCOUNTERED.    SENERAL HAINTENANCE WAS PERFORMED ON THE FGD SYSTEM DURING THE FOURTH QUARTER. NO FGD FORCED OUTAGES WERE ENCOUNTERED.    SENERAL HAINTENANCE WAS PERFORMED ON THE FGD SYSTEM DURING THE FOURTH QUARTER. NO FGD FORCED OUTAGES WERE ENCOUNTERED.    SENERAL HAINTENANCE WAS PERFORMED ON THE FGD SYSTEM DURING THE FOURTH QUARTER. NO FGD FORCED OUTAGES WERE ENCOUNTERED.    SENERAL HAINTENANCE WAS PERFORMED ON THE FGD SYSTEM DURING THE FOURTH QUARTER. NO FGD OUTAGES WERE ENCOUNTERED.    SENERAL HAINTENANCE WAS PERFORMED ON THE FGD SYSTEM DURING THE FOURTH QUARTER DURING THE FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST QUARTER OF 1982.		23		76.6		76.6						
SYSTEM 75.9 75.9 76.9 744 744 565 83.  L/81 21 26.4 26.4 26.4 26.4 22 91.9 91.9 91.9 23 68.1 68.1 24 80.3 80.3 80.3 80.3 80.3 80.3 80.3 80.3		24		85.7								
22 91.9 91.9 91.0 23 68.1 68.1 68.1 24 80.3 80.3 80.3 5YSTEM 66.7 66.7 66.7 720 720 480 67. 2781 24 77.2 77.1 22 77.1 22 77.1 22 77.1 23 70.8 70.8 70.7 24 63.3 63.2 5YSTEM 66.9 66.8 744 743 497 68. *** PROBLEMS/SOLUTIONS/COMMENTS		SYSTEM							744	744	565	83.6
22 91.9 91.9 91.0 23 68.1 68.1 68.1 24 80.3 80.3 80.3 5YSTEM 66.7 66.7 66.7 720 720 480 67. 2781 24 77.2 77.1 22 77.1 22 77.1 22 77.1 23 70.8 70.8 70.7 24 63.3 63.2 5YSTEM 66.9 66.8 744 743 497 68. *** PROBLEMS/SOLUTIONS/COMMENTS	1/81	21		26.4		26.4						
23 68.1 68.1 24 80.3 80.3 80.3 80.3 80.3 80.3 80.3 80.3												
24 80.3 80.3 80.3 80.3 5  SYSTEM 66.7 66.7 7.20 720 480 67.  2281 21 77.2 77.1 22 77.1 24 63.3 63.2 66.8 744 743 497 68.  *** PROBLEMS/SOLUTIONS/COMMENTS   GENERAL MAINTENANCE HAS PERFORMED ON THE FGD SYSTEM DURING THE FOURTH QUARTER. NO FGD FORCED OUTAGES WERE ENCOUNTERED.  *** PROBLEMS/SOLUTIONS/COMMENTS  GENERAL MAINTENANCE HAS PERFORMED ON THE FGD SYSTEM DURING THE FOURTH QUARTER. NO FGD FORCED OUTAGES WERE ENCOUNTERED.  *** PROBLEMS/SOLUTIONS/COMMENTS  *** PROBLEMS/SOLUTIONS/COMMENTS  *** 100.0 82.4 100.0 82.3 23 22 100.0 92.9 100.0 92.7 24 100.0 63.0 100.0 62.9 37.2 744 743 545 79.  *** 24 100.0 63.0 100.0 62.9 73.2 744 743 545 79.  *** 25 100.0 65.9 100.0 85.6 22 100.0 65.6 23 100.0 93.5 100.0 93.2 24 100.0 86.2 100.0 85.9 57.5 73.  *** 26 21 100.0 82.9 100.0 82.6 672 670 555 73.  *** 21 100.0 93.6 100.0 82.9 100.0 82.6 672 670 555 73.  *** 22 100.0 61.5 100.0 82.9 100.0 82.6 672 670 555 73.  *** SYSTEM 100.0 54.3 100.0 51.2 31 100.0 63.0 744 702 448 65.  *** PROBLEMS/SOLUTIONS/COMMENTS  *** PROBLEMS/SOLUTIONS/COMMENTS  *** PROBLEMS/SOLUTIONS/COMMENTS  *** PROBLEMS/SOLUTIONS/COMMENTS												
SYSTEM 66.7 66.7 720 720 480 67.  2781 21 77.2 77.1 22 56.2 56.1 23 70.8 70.8 70.7 24 63.3 63.2 SYSTEM 66.9 66.8 744 743 497 68.  ** PROBLEMS/SOLUTIONS/COMMENTS   GENERAL MAINTENANCE HAS PERFORMED ON THE FGD SYSTEM DURING THE FOURTH QUARTER. NO FGD FORCED OUTAGES WERE ENCOUNTERED.  1.782 21 100.0 82.4 100.0 82.3 22 100.0 54.9 100.0 54.8 23 100.0 92.9 100.0 92.7 24 100.0 63.0 100.0 62.9 SYSTEM 100.0 73.3 100.0 73.2 744 743 545 79.  2.782 21 100.0 85.9 100.0 85.6 22 100.0 65.9 100.0 85.6 23 100.0 93.5 100.0 93.2 24 100.0 86.2 100.0 85.9 SYSTEM 100.0 86.2 100.0 85.9 SYSTEM 100.0 82.9 100.0 82.6 672 670 555 73.  3.782 21 100.0 93.6 100.0 82.6 672 670 555 73.  3.783 21 100.0 93.6 100.0 82.6 672 670 555 73.  3.784 21 100.0 86.2 100.0 82.9 100.0 82.6 672 670 555 73.  3.785 21 100.0 93.6 100.0 82.9 100.0 82.6 672 670 555 73.  3.787 21 100.0 93.6 100.0 82.9 100.0 82.6 672 670 555 73.  3.788 21 100.0 93.6 100.0 82.9 100.0 82.6 672 670 555 73.  3.789 21 100.0 93.6 100.0 83.3 744 702 448 65.  3.789 31 500.0 46.0 100.0 58.1 74. 702 448 65.  3.789 31 500.0 46.0 100.0 60.3 744 702 448 65.  3.789 31 500.0 61.5 100.0 60.3 744 702 448 65.												
2/81 21 77.2 77.1 22 56.2 56.1 23 70.8 70.7 24 63.3 63.2 SYSTEM 66.9 66.8 744 743 497 68.  ** PROBLEMS/SOLUTIONS/COMMENTS   GENERAL MAINTENANCE WAS PERFORMED ON THE FGD SYSTEM DURING THE FOURTH QUARTER. NO FGD FORCED OUTAGES WERE ENCOUNTERED.  1/82 21 100.0 82.4 100.0 82.3 22 100.0 54.9 100.0 54.8 23 100.0 92.9 100.0 92.7 24 100.0 63.0 100.0 62.9 SYSTEM 100.0 63.0 100.0 62.9 SYSTEM 100.0 85.9 100.0 85.6 22 100.0 65.9 100.0 85.6 22 100.0 65.9 100.0 85.9 SYSTEM 100.0 86.2 100.0 85.9 SYSTEM 100.0 66.2 100.0 85.9 SYSTEM 100.0 66.3 100.0 88.3 22 100.0 61.5 100.0 88.3 24 100.0 93.6 100.0 88.3 25 100.0 93.6 100.0 88.3 26 100.0 93.6 100.0 88.3 27 100.0 93.6 100.0 88.3 28 100.0 93.6 100.0 88.3 SYSTEM 100.0 63.9 100.0 60.3 744 702 448 65.  ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR PROBLEMS OR FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST QUARTER OF 1982.									720	720	480	47 4
22 56.2 56.1 23 70.8 70.7 24 63.3 63.2 SYSTEM 66.9 66.8 744 743 497 68.  *** PROBLEMS/SOLUTIONS/COMMENTS  GENERAL MAINTENANCE WAS PERFORMED ON THE FGD SYSTEM DURING THE FOURTH QUARTER. NO FGD FORCED OUTAGES WERE ENCOUNTERED.  1/82 21 100.0 82.4 100.0 82.3 22 100.0 54.9 100.0 54.8 23 100.0 92.9 100.0 92.7 24 100.0 63.0 100.0 62.9 SYSTEM 100.0 73.3 100.0 73.2 744 743 545 79.  2/82 21 100.0 85.9 100.0 85.6 22 100.0 65.9 100.0 85.6 23 100.0 93.5 100.0 93.2 24 100.0 86.2 100.0 85.9 SYSTEM 100.0 86.1 100.0 82.6 672 670 555 73.  1/82 21 100.0 93.6 100.0 88.3 24 100.0 93.6 100.0 88.3 25 100.0 93.6 100.0 88.3 26 100.0 93.6 100.0 88.3 27 100.0 93.6 100.0 88.3 28 100.0 93.6 100.0 88.3 29 100.0 93.6 100.0 88.3 20 100.0 93.6 100.0 88.3 21 100.0 93.6 100.0 88.3 22 100.0 61.5 100.0 58.1 23 100.0 93.6 100.0 58.1 24 100.0 54.3 100.0 58.1 25 100.0 61.5 100.0 58.1 26 100.0 54.3 100.0 51.2 SYSTEM 100.0 54.3 100.0 51.2 SYSTEM 100.0 54.3 100.0 60.3 744 702 448 65.  ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR PROBLEMS OR FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST QUARTER OF 1982.	0 (03	••							720	720	400	07.4
23 70.8 70.7 24 63.3 63.2 SYSTEM 66.9 66.8 744 743 497 68.  *** PROBLEMS/SOLUTIONS/COMMENTS  GENERAL MAINTENANCE WAS PERFORMED ON THE FGD SYSTEM DURING THE FOURTH QUARTER. NO FGD FORCED OUTAGES WERE ENCOUNTERED.  1/82 21 100.0 82.4 100.0 54.8 23 100.0 54.9 100.0 54.8 23 100.0 62.9 100.0 62.9 SYSTEM 100.0 63.0 100.0 62.9 SYSTEM 100.0 65.9 100.0 62.9 SYSTEM 100.0 85.9 100.0 65.6 22 100.0 65.9 100.0 65.6 23 100.0 93.5 100.0 93.2 24 100.0 86.2 100.0 85.9 SYSTEM 100.0 82.9 100.0 85.9 SYSTEM 100.0 82.9 100.0 85.9 SYSTEM 100.0 66.0 100.0 85.9 SYSTEM 100.0 63.9 100.0 86.3 SYSTEM 100.0 63.9 100.0 86.3 SYSTEM 100.0 63.9 100.0 60.3 744 702 448 65.  *** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR PROBLEMS OR FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST QUARTER OF 1982.	2/81											
24 63.3 63.2   SYSTEM 66.9 66.8 744 743 497 68.  *** PROBLEMS/SOLUTIONS/COMMENTS  GENERAL MAINTENANCE WAS PERFORMED ON THE FGD SYSTEM DURING THE FOURTH QUARTER. NO FGD FORCED OUTAGES WERE ENCOUNTERED.  1/82 21 100.0 82.4 100.0 82.3 23 100.0 92.9 100.0 92.7 24 100.0 63.0 100.0 62.9 27.2 24 100.0 73.3 100.0 73.2 744 743 545 79.  2/82 21 100.0 85.9 100.0 85.6 22 100.0 85.9 27.2 24 100.0 85.9 100.0 85.6 23 100.0 93.5 100.0 93.2 24 100.0 86.2 100.0 85.9 SYSTEM 100.0 86.2 100.0 85.9 SYSTEM 100.0 93.5 100.0 93.2 24 100.0 86.2 100.0 85.9 SYSTEM 100.0 82.9 100.0 82.6 672 670 555 73.  3/82 21 100.0 93.6 100.0 82.9 100.0 82.6 672 670 555 73.  3/82 21 100.0 93.6 100.0 88.3 22 100.0 61.5 100.0 82.6 672 670 555 73.  3/82 21 100.0 93.6 100.0 88.3 22 100.0 61.5 100.0 82.6 672 670 555 73.  3/83 24 100.0 61.5 100.0 58.1 23 100.0 44.0 100.0 43.4 24 100.0 54.3 100.0 54.3 100.0 54.3 100.0 54.3 SYSTEM 100.0 63.9 100.0 60.3 744 702 448 65.  *** PROBLEMS/SOLUTIONS/COMMENTS  *** PROBLEMS/SOLUTIONS/COMMENTS  *** PROBLEMS/SOLUTIONS/COMMENTS												
SYSTEM 66.9 66.8 744 743 497 68.  *** PROBLEMS/SOLUTIONS/COMMENTS  GENERAL MAINTENANCE WAS PERFORMED ON THE FGD SYSTEM DURING THE FOURTH QUARTER. NO FGD FORCED OUTAGES WERE ENCOUNTERED.  1.782 21 100.0 82.4 100.0 82.3 23 100.0 92.9 100.0 92.7 24 100.0 63.0 100.0 62.9 575TEM 100.0 63.0 100.0 62.9 575TEM 100.0 63.0 100.0 65.6 22 100.0 85.9 100.0 85.6 22 100.0 85.9 100.0 85.6 22 100.0 86.2 100.0 85.9 575TEM 100.0 93.5 100.0 93.2 24 100.0 86.2 100.0 85.9 575TEM 100.0 86.3 100.0 82.6 672 670 555 73. 100.0 93.6 100.0 82.6 672 670 555 73. 100.0 93.6 100.0 83.1 100.0 93.6 100.0 88.3 100.0 93.5 100.0 93.2 100.0 93.6 100.0 93.6 100.0 93.6 100.0 93.6 100.0 86.0 93.0 93.0 93.0 93.0 93.0 93.0 93.0 93						70.7						
** PROBLEMS/SOLUTIONS/COMMENTS  GENERAL MAINTENANCE WAS PERFORMED ON THE FGD SYSTEM DURING THE FOURTH QUARTER. NO FGD FORCED OUTAGES WERE ENCOUNTERED.  1.782 21				63.3		63.2						
GENERAL MAINTENANCE WAS PERFORMED ON THE FGD SYSTEM DURING THE FOURTH QUARTER. NO FGD FORCED OUTAGES WERE ENCOUNTERED.  1/82 21		SYSTEM		66.9		66.8			744	743	497	68.8
QUARTER. NO FGD FORCED OUTAGES WERE ENCOUNTERED.  1/82 21		** PROB	LEMS/SOLUTION	NS/COMMENTS								
22 100.0 54.9 100.0 54.8 23 100.0 92.9 100.0 92.7 24 100.0 63.0 100.0 62.9 SYSTEM 100.0 73.3 100.0 73.2 744 743 545 79. 2782 21 100.0 85.9 100.0 85.6 22 100.0 65.9 100.0 65.6 23 100.0 93.5 100.0 93.2 24 100.0 86.2 100.0 85.9 SYSTEM 100.0 86.2 100.0 85.9 SYSTEM 100.0 86.2 100.0 85.9 SYSTEM 100.0 82.9 100.0 82.6 672 670 555 73. 3782 21 100.0 93.6 100.0 82.6 672 670 555 73. 3883 22 100.0 61.5 100.0 58.1 23 100.0 46.0 100.0 43.4 24 100.0 54.3 100.0 54.3 SYSTEM 100.0 54.3 100.0 51.2 SYSTEM 100.0 63.9 100.0 60.3 744 702 448 65. ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR PROBLEMS OR FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST QUARTER OF 1982.			G Q	ENERAL MAINTE UARTER. NO F	NANCE WAS P	ERFORMED ON T	HE FGD	SYSTE	M DURI	NG THE	FOURTH	l
22 100.0 54.9 100.0 54.8 23 100.0 92.9 100.0 92.7 24 100.0 63.0 100.0 62.9 SYSTEM 100.0 73.3 100.0 73.2 744 743 545 79. 2782 21 100.0 85.9 100.0 85.6 22 100.0 65.9 100.0 65.6 23 100.0 93.5 100.0 93.2 24 100.0 86.2 100.0 85.9 SYSTEM 100.0 86.2 100.0 85.9 SYSTEM 100.0 86.2 100.0 85.9 SYSTEM 100.0 82.9 100.0 82.6 672 670 555 73. 3782 21 100.0 93.6 100.0 82.6 672 670 555 73. 3883 22 100.0 61.5 100.0 58.1 23 100.0 46.0 100.0 43.4 24 100.0 54.3 100.0 54.3 SYSTEM 100.0 54.3 100.0 51.2 SYSTEM 100.0 63.9 100.0 60.3 744 702 448 65. ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR PROBLEMS OR FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST QUARTER OF 1982.	1/82	21	100.0	82.4	100.0	82.3						
23 100.0 92.9 100.0 92.7 24 100.0 63.0 100.0 62.9 SYSTEM 100.0 73.3 100.0 73.2 744 743 545 79.  27/82 21 100.0 85.9 100.0 85.6 22 100.0 65.6 23 100.0 93.5 100.0 93.2 24 100.0 86.2 100.0 85.9 SYSTEM 100.0 82.9 100.0 85.9 SYSTEM 100.0 82.9 100.0 82.6 672 670 555 73.  28/82 21 100.0 93.6 100.0 82.6 672 670 555 73.  29/82 21 100.0 93.6 100.0 88.3 22 100.0 61.5 100.0 58.1 23 100.0 61.5 100.0 58.1 23 100.0 61.5 100.0 58.1 23 100.0 63.9 100.0 63.9 100.0 60.3 744 702 448 65.  ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR PROBLEMS OR FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST QUARTER OF 1982.			100.0	54.9	100.0							
24 100.0 63.0 100.0 62.9  SYSTEM 100.0 73.3 100.0 73.2 744 743 545 79.  2/82 21 100.0 85.9 100.0 85.6  22 100.0 65.9 100.0 93.2  24 100.0 86.2 100.0 85.9  SYSTEM 100.0 82.9 100.0 82.6 672 670 555 73.  3/82 21 100.0 93.6 100.0 88.3  22 100.0 61.5 100.0 58.1  23 100.0 46.0 100.0 58.1  23 100.0 46.0 100.0 43.4  24 100.0 54.3 100.0 51.2  SYSTEM 100.0 63.9 100.0 60.3 744 702 448 65.  ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR PROBLEMS OR FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST QUARTER OF 1982.		23		92.9	100.0							
SYSTEM 100.0 73.3 100.0 73.2 744 743 545 79.  2/82 21 100.0 85.9 100.0 85.6 22 100.0 65.9 100.0 65.6 23 100.0 93.5 100.0 93.2 24 100.0 86.2 100.0 85.9 SYSTEM 100.0 82.9 100.0 82.6 672 670 555 73.  2/82 21 100.0 93.6 100.0 88.3 22 100.0 61.5 100.0 58.1 23 100.0 46.0 100.0 58.1 23 100.0 46.0 100.0 43.4 24 100.0 54.3 100.0 51.2 SYSTEM 100.0 63.9 100.0 60.3 744 702 448 65.  *** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR PROBLEMS OR FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST QUARTER OF 1982.				63.0								
2/82 21 100.0 85.9 100.0 85.6 22 100.0 65.9 100.0 65.6 23 100.0 93.5 100.0 93.2 24 100.0 86.2 100.0 85.9 SYSTEM 100.0 82.9 100.0 82.6 672 670 555 73.  3/82 21 100.0 93.6 100.0 88.3 22 100.0 61.5 100.0 58.1 23 100.0 46.0 100.0 58.1 23 100.0 46.0 100.0 43.4 24 100.0 54.3 100.0 51.2 SYSTEM 100.0 63.9 100.0 60.3 744 702 448 65.  *** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR PROBLEMS OR FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST QUARTER OF 1982.									744	743	545	79.4
22 100.0 65.9 100.0 65.6 23 100.0 93.5 100.0 93.2 24 100.0 86.2 100.0 85.9 SYSTEM 100.0 82.9 100.0 82.6 672 670 555 73.  3/82 21 100.0 93.6 100.0 88.3 22 100.0 61.5 100.0 58.1 23 100.0 46.0 100.0 43.4 24 100.0 54.3 100.0 51.2 SYSTEM 100.0 63.9 100.0 60.3 744 702 448 65.  ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR PROBLEMS OR FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST QUARTER OF 1982.	2/82	21										
23 100.0 93.5 100.0 93.2 24 100.0 86.2 100.0 85.9 SYSTEM 100.0 82.9 100.0 82.6 672 670 555 73.  3/82 21 100.0 93.6 100.0 88.3 22 100.0 61.5 100.0 58.1 23 100.0 46.0 100.0 43.4 24 100.0 54.3 100.0 51.2 SYSTEM 100.0 63.9 100.0 60.3 744 702 448 65.  ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR PROBLEMS OR FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST QUARTER OF 1982.												
24 100.0 86.2 100.0 85.9 SYSTEM 100.0 82.9 100.0 82.6 672 670 555 73.  3/82 21 100.0 93.6 100.0 88.3 22 100.0 61.5 100.0 58.1 23 100.0 46.0 100.0 43.4 24 100.0 54.3 100.0 51.2 SYSTEM 100.0 63.9 100.0 60.3 744 702 448 65.  ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR PROBLEMS OR FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST QUARTER OF 1982.												
SYSTEM 100.0 82.9 100.0 82.6 672 670 555 73.  5/82 21 100.0 93.6 100.0 88.3 22 100.0 61.5 100.0 58.1 23 100.0 46.0 100.0 43.4 24 100.0 54.3 100.0 51.2 SYSTEM 100.0 63.9 100.0 60.3 744 702 448 65.  ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR PROBLEMS OR FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST QUARTER OF 1982.						93.2						
3/82 21 100.0 93.6 100.0 88.3 22 100.0 61.5 100.0 58.1 23 100.0 46.0 100.0 43.4 24 100.0 54.3 100.0 51.2 SYSTEM 100.0 63.9 100.0 60.3 744 702 448 65.  ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR PROBLEMS OR FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST QUARTER OF 1982.					100.0	85.9						
22 100.0 61.5 100.0 58.1 23 100.0 46.0 100.0 43.4 24 100.0 54.3 100.0 51.2 SYSTEM 100.0 63.9 100.0 60.3 744 702 448 65.  ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR PROBLEMS OR FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST QUARTER OF 1982.		SYSTEM	100.0	82.9	100.0	82.6			672	670	<b>5</b> 55	73.8
22 100.0 61.5 100.0 58.1 23 100.0 46.0 100.0 43.4 24 100.0 54.3 100.0 51.2 SYSTEM 100.0 63.9 100.0 60.3 744 702 448 65.  ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR PROBLEMS OR FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST QUARTER OF 1982.	3/82	21	100.0	93.6	100.0	88.3						
23 100.0 46.0 100.0 43.4 24 100.0 54.3 100.0 51.2 SYSTEM 100.0 63.9 100.0 60.3 744 702 448 65.  ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR PROBLEMS OR FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST QUARTER OF 1982.		22	100.0									
24 100.0 54.3 100.0 51.2 SYSTEM 100.0 63.9 100.0 60.3 744 702 448 65.  ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR PROBLEMS OR FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST QUARTER OF 1982.		23										
SYSTEM 100.0 63.9 100.0 60.3 744 702 448 65.  ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR PROBLEMS OR FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST QUARTER OF 1982.												
** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR PROBLEMS OR FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST  QUARTER OF 1982.									744	702	448	65.3
NO MAJOR PROBLEMS OR FORCED OUTAGES WERE ENCOUNTERED DURING THE FIRST QUARTER OF 1982.		** PROB	LEMS/SOLUTION			23.0			, 77	702	740	03.3
QUARTER OF 1982.					FMS OD FODC	EN DITAGES HE	DE ENG	OINTER	En nim	TUC		
/82 21 60.3 60.3 100.0 60.3			QU	JARTER OF 198	2.	LU GUTAGES ME	KE ENL	JUNIER	נבט טעR	TNG THE	: FIRST	
	+/82	21	60.3	60.3	100.0	60.3						

720

9/83 SYSTEM

		AVAILABILITY		RELIABILITY	UTILIZATIO	N % REMOVA \$02 PAR	L PER	BOILER HOURS	HOURS	FACTOR
	22		42.6							
	23	95.6	83.2	100.0	83.2					
	24	99.7	83.2 86.7	100.0	86.7					
	SYSTEM	74.8	68.2	100.0	68.2		720	720	491	73.1
5/82	21	98.6	72.0 32.7	100.0 100.0	71.9					
	22	87.2	32.7	100.0	32.7					
	23	64.5 36.3	28.0	100.0 100.0	27.9					
	24	36.3	7.0							
	SYSTEM	71.6	34.9	100.0	34.9		744	743	260	64.9
6/82	21	87.8	39.4 47.5	100.0	39.3					
	22	90.3	47.5	100.0	47.4					
	23	100.0 96.4	87.3	100.0	87.1					
	24	96.4	53.9	100.0	53.7					
	SYSTEM	93.6	57.0	100.0	56.9		720	718	409	64.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS							
			URING THE SE				NCE AND C	CLEANING	OF TI	HE
7/82	SYSTEM						744			
8/82	SYSTEM						744			
9/82	SYSTEM						720			
10/82	SYSTEM						744			
11/82	SYSTEM						720			
12/82	SYSTEM						744			
1/83	SYSTEM						744			
	SYSTEM						672			
3/83	SYSTEM						744			
	** PRU	BLEMS/SOLUTIC	NFORMATION W	AC INIAVATIAE	NE EOD THE	DEDION OF	IIII Y 1982	THROUGH	H MADC	דמפו ע
4/87	SYSTEM		INFURNATION W	AS UNAVAILAD	SEE FOR THE	FERIOD OF S	720	mkoodi	II HARC	11 1705.
	SYSTEM						744			
	SYSTEM						720			
		BLEMS/SOLUTIO	NS/COMMENTS							
	, i, <b>o</b>		NFORMATION W	AS UNAVAILAE	BLE FOR THE	PERIOD OF .	JULY 1982	THROUG	н Јиме	1983.
7/83	SYSTEM						744			
8/83	SYSTEM						744			

COOPERATIVE POWER ASSOCIATION: COAL CREEK 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE THIRD QUARTER OF 1983.

 10/83
 SYSTEM
 744

 11/83
 SYSTEM
 720

 12/83
 SYSTEM
 744

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE FGD SYSTEM AT COAL CREEK 2 WAS 100 PERCENT AVAILABLE THROUGHOUT THE FOURTH QUARTER OF 1983.

1/84	SYSTEM	744
2/84	SYSTEM	696
3/84	SYSTEM	744
4/84	SYSTEM	720
5/84	SYSTEM	744

### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE SCHEDULED OUTAGE IN MAY, CORRODING REHEAT DUCTWORK WAS REPLACED WITH STAINLESS STEEL.

6/84 SYSTEM 720 7/84 SYSTEM 744

### ** PROBLEMS/SOLUTIONS/COMMENTS

FGD SYSTEM AVAILABILITY DURING THE PERIOD OF JANUARY THROUGH JULY WAS REPORTED AS 100%.

 8/84
 SYSTEM
 744

 9/84
 SYSTEM
 720

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED REPLACING DETERIORATING MIST ELIMINATOR FIBERGLASS LININGS DURING THE FIRST THREE QUARTERS OF 1984.

# SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

______ DELMARVA POWER & LIGHT COMPANY NAME PLANT NAME DELAWARE CITY UNIT NUMBER CITY DELAWARE CITY STATE DELAWARE REGULATORY CLASSIFICATION PARTICULATE EMISSION LIMITATION - NG/J 129. ( .300 LB/MMBTU) SO2 EMISSION LIMITATION - NG/J (**** LB/MMBTU) ***** NOX EMISSION LIMITATION - NG/J ***** (***** LB/MMBTU) NET PLANT GENERATING CAPACITY - MW 180 GROSS UNIT GENERATING CAPACITY - MW 60 NET UNIT GENERATING CAPACITY W/FGD - MW 495 NET UNIT GENERATING CAPACITY WO/FGD - MW 495 EQUIVALENT SCRUBBED CAPACITY - MW ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER RILEY STOKER BOILER TYPE PULVERIZED COAL BOILER SERVICE LOAD BASE DESIGN BOILER FLUE GAS FLOW CU.M/S 139.21 215.6 152. ( 295000 ACFM) BOILER FLUE GAS TEMPERATURE - C ( 420 F) STACK HEIGHT - M ( 500 FT) STACK SHELL CONCRETE STACK TOP DIAMETER - M 6.1 ( 20.0 FT) ** FUEL DATA FUEL TYPE COKE FUEL GRADE BITUMINOUS AVERAGE HEAT CONTENT - J/G ( 14000 BTU/LB) 32564. RANGE HEAT CONTENT - BTU/LB 13500-14500 AVERAGE ASH CONTENT - % .50 RANGE ASH CONTENT - % 0.3-0.7 AVERAGE MOISTURE CONTENT - % . 70 RANGE MOISTURE CONTENT - % 0.5-1.2 AVERAGE SULFUR CONTENT - % 7.00 RANGE SULFUR CONTENT - % 5.0-8.0 AVERAGE CHLORIDE CONTENT - % ****** RANGE CHLORIDE CONTENT - % ***** *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER 3 TYPE TUBULAR SUPPLIER PRAT-DANIEL PARTICLE REMOVAL EFFICENCY -% 92.0 ** FABRIC FILTER NUMBER n NONE ( 2.0 FT/MIN) TYPICAL GAS/CLOTH RATIO - M/MIN .6 ** ESP NUMBER COLD SIDE TYPE WESTERN PREC. DIVISION, JOY SUPPLIER 34.8 ( 73700 ACFM) 54.4 ( 130 F) .2 ( 1. IN-H2O) INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE - C FRESSURE DROP - KPA 95.0 PARTICLE REMOVAL EFFICENCY - % ** PARTICLE SCRUBBER NUMBER 4/80 INITIAL START-UP DATE GENERIC TYPE VENTURI TOWER VARIABLE-THROAT/BOTTOM-ENTRY PLUMB BOB SPECIFIC TYPE TRADE NAME/COMMON NAME N/A AIRPOL SUPPLIER. DIMENSIONS - FT 20 DIA X 70.0

### DELMARVA POWER & LIGHT: DELAWARE CITY 1 (CONT.)

```
CARBON STEEL
    SHELL GENERIC MATERIAL
                                               AISI 1110
    SHELL SPECIFIC MATERIAL
                                               ORGANIC; INORGANIC
    LINER GENERIC MATERIAL
                                               GLASS FLAKE-FILLED POLYESTER; PREFIRED BRICK/SHA
    LINER SPECIFIC MATERIAL
                                               NONE
    GAS CONTACTING DEVICE TYPE
                                               1
    NUMBER OF CONTACTING ZONES
                                               315.0
                                                            ( 5000 GPM)
(50.9 GAL/1000ACF)
    LIQUID RECIRCULATION RATE - LITER/S
                                                 6.8
    L/G RATIO - LITER/CU.M
                                                             ( 2.0 IN-H20)
    PRESSURE DROP - KPA
                                                    .5
                                                             ( 98300 ACFM)
( 430 F)
                                                 46.4
    INLET GAS FLOW RATE - CU.M/S
    INLET GAS TEMPERATURE - C
SO2 REMOVAL EFFICENCY - %
                                                 221.1
                                                  . 0
                                                  81.5
    PARTICLE REMOVAL EFFICIENCY - %
*** FGD SYSTEM
** GENERAL DATA
                                               SALEABLE PRODUCT
    SALEABLE PRODUCT/THROWAWAY PRODUCT
                                               WET SCRUBBING
    SO2 REMOVAL MODE
                                               WELLMAN LORD
    PROCESS TYPE
                                               DAVY MCKEE
    SYSTEM SUPPLIER
                                               DAVY MCKEE
    A-E FIRM
                                               FULL SCALE
    DEVELOPMENT LEVEL
                                               RETROFIT
    NEW/RETROFIT
    UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 90.00
    UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
    CURRENT STATUS
                                                5/80
    COMMERCIAL START-UP
    INITIAL START-UP
                                                5/80
    CONTRACT AWARDED
                                                9/77
 ** DESIGN AND OPERATING PARAMETERS
    SPACE REQUIREMENTS - SQ M
                                             24280.3 ( 261360 SQ FT)
    OPER. & MAINT, REQUIREMENT - MANHR/DAY
                                               144.0
 ** QUENCHER/PRESATURATOR
    CONSTRUCTION MATERIAL GENERIC TYPE
                                              ИD
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               NR
 ** ABSORBER
    NUMBER
                                                3
    NUMBER OF SPARES
                                                0
    GENERIC TYPE
                                               TRAY TOWER
    SPECIFIC TYPE
                                               VALVE TRAY
    TRADE NAME/COMMON TYPE
                                               BUBBLE CAP TRAY TOWER
    SUPPLIER
                                               DAVY MCKEE
    DIMENSIONS FT
                                               20.0 X 20.0
    SHELL GENERIC MATERIAL
                                               INORGANIC
    SHELL SPECIFIC MATERIAL
                                               HYDRAULICALLY-BONDED CONCRETE
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                               PORTLAND CEMENT
    LINER GENERIC MATERIAL
                                               INORGANIC
    LINER SPECIFIC MATERIAL
                                               PREFIRED BRICK/SHAPES
     LINER MATERIAL TRADE NAME/COMMON TYPE
                                               ИÞ
    GAS CONTACTING DEVICE TYPE
                                               VALVE TRAY
    NUMBER OF CONTACTING ZONES
     LIQUID PECIRCULATION RATE - LITER/S
                                                             ( 400 GPM)
                                                   .7
     L/G RATIO L/CU.M
                                                            ( 5.5 GAL/1000 ACF)
( 73300 ACFM)
( 130 F)
     INLET GAS FLOW - CU. M/S
                                                  34.59
     INLET GAS TEMPERATURE - C
                                                  54.4
    PARTICLE REMOVAL EFFICENCY - %
                                                    .0
 ** MIST ELIMINATOR
    PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                               PRIMARY COLLECTOR
    NUMBER PER SYSTEM
                                                3
    GENERIC TYPE
                                               IMPINGEMENT
    SPECIFIC TYPE
                                               BAFFLE
    TRADE NAME/COMMON TYPE
                                               CLOSED VANE
    CONFIGURATION
                                               HORIZONTAL
    NUMBER OF STAGES
                                                   1
    NUMBER OF PASSES PER STAGE
                                                   1
    FREEBOARD DISTANCE M
                                                   1.83
                                                             ( 6.0 FT)
```

#### DELMARVA POWER & LIGHT: DELAWARE CITY 1 (CONT.)

```
DISTANCE BETWEEN STAGES - CM
                                                   19.05
                                                               ( 7.5 IN)
    PRESSURE DROP - KPA
                                                     .1
                                                                  .3 IN-H2O)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                ORGANIC
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                POLYPHENYLENE
    WASH WATER SOURCE
                                                COOLED CONDENSATE
    WASH FREQUENCY
                                                INTERMITTENT
    WASH RATE - L/S
                                                    3.2
                                                               ( 50 GAL/MIN)
** REHEATER
    NUMBER
    GENERIC TYPE
                                                DIRECT COMBUSTION
    SPECIFIC TYPE
                                                EXTERNAL COMBUSTION CHAMBER
    TRADE NAME/COMMON TYPE
                                                NATURAL GAS
    TEMPERATURE INCREASE - C
                                                   27.8
                                                                   50 F)
    INLET FLUE GAS FLOW RATE - CU. M/S
                                                  108.54
                                                               ( 230000 ACFM)
    INLET FLUE GAS TEMPERATURE - C
                                                  54.4
                                                               ( 130 F)
    OUTLET FLUE GAS TEMPERATURE - C
                                                  85.0
                                                               ( 185 F)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                NR
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                ND
** FANS
    NUMBER
                                                 3
    NUMBER OF SPARES
                                                 0
    DESIGN
                                                CENTRIFUGAL
    SUPPLIER
                                                ROBINSON
    FUNCTION
                                                BOOSTER
    APPLICATION
                                                INDUCED DRAFT
    SERVICE
                                                DRY
    FLUE GAS FLOW RATE - CU.M/S
                                                 139.21
                                                              ( 295000 ACFM)
    FLUE GAS TEMPERATURE - C
                                                               ( 420 F)
                                                  215.6
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL
** DAMPERS
    FUNCTION
                                                NR
    GENERIC TYPE
                                                NR
    SPECIFIC TYPE
                                                NR
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                NR
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                NR
    LINER GENERIC MATERIAL TYPE
                                                NR
    LINER SPECIFIC MATERIAL TYPE
                                                NR
** DUCTWORK
    DIMENSIONS
                                                8.0 X 8.0
     SHELL GENERIC MATERIAL TYPE
                                                CARBON STEEL
     SHELL SPECIFIC MATERIAL TYPE
                                                AISI 1110
     LINER GENERIC MATERIAL TYPE
                                                ORGANIC
     LINER SPECIFIC MATERIAL TYPE
                                                FIBER-REINFORCED POLYESTER
** REAGENT PREPARATION EQUIPMENT
    FUNCTION
                                                MIX TANK
    DEVICE
                                                N/A
    DEVICE TYPE
                                                AGITATED TANK
 ** TANKS
    SERVICE
                                                NUMBER
    -----
                                                -----
                                                ****
    NR
 ** PUMPS
    SERVICE
                                                NUMBER
                                                ****
    ABSORBER RECIRCULATION
** SOLIDS CONCENTRATING/DEWATERING
                                                NONE
    DEVICE
*** SALEABLE BYPRODUCTS
                                                SULFURIC ACID
                                                               ( 12.50 TPH)
    FULL LOAD QUANTITY - M T/H
                                                   11.34
```

DELMARVA POWER & LIGHT: DELAWARE CITY 1 (CONT.)

93.0 QUALITY 7. MARKETED DISPOSITION

*** SLUDGE

** TREATMENT

N/A METHOD N/A DEVICE PROPRIETARY PROCESS N/A

** DISPOSAL

FINAL NATURE POND TYPE

CLAY LINING SITE TREATMENT

** PROCESS CONTROL AND INSTRUMENTATION

PH, SOLIDS, SP.G., CONC. CHEMICAL PARAMETERS GAS OUTLET, SOLUTION OUTLET MONITOR LOCATION AUTOMATIC PROCESS CONTROL MANNER PROCESS CHEMISTRY MODE FEEDBACK

** WATER BALANCE

5/80 SYSTEM

CLOSED WATER LOOP TYPE

100.0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS FACTOR

100.0 ** PROBLEMS/SOLUTIONS/COMMENTS

> THE FGD SYSTEM BEGAN INITIAL AND COMMERCIAL OPERATIONS ON MAY 22, 1980. NO MAJOR PROBLEMS WERE ENCOUNTERED FROM STARTUP THROUGH THE END OF THE MONTH.

744

240

240

32.3

6/80 SYSTEM 98.9 98.9 98.9 98.9 720 720 712

100.0

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR PROBLEMS WERE ENCOUNTERED DURING JUNE.

7/80 SYSTEM 97.2 97.0 97.0 90.7 744 696 675

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS DOWN FOR PART OF THE MONTH IN JULY TO REPAIR A LEAK IN THE MIST ELIMINATOR.

8/80 SYSTEM 99.9 99.9 99.9 99.9 744 744 743

** PROBLEMS/SOLUTIONS/COMMENTS

NO FGD-RELATED PROBLEMS WERE REPORTED DURING AUGUST.

9/80 SYSTEM 78.3 78.3 78.3 78.3 720. 720 564

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS OFF LINE DURING SEPTEMBER DUE TO NECESSARY REPAIR OF THE CIRCULATING PUMPS AND THE MIST ELIMINATOR.

FGD SYSTEM OUTAGE TIME OCCURRED DUE TO INLET DUCT EXPANSION JOINT REPAIRS.

10/80 SYSTEM 66.1 66.1 66.1 66.1 744 744 492 DELMARVA POWER & LIGHT: DELAWARE CITY 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

_____

** PROBLEMS/SOLUTIONS/COMMENTS

DURING OCTOBER SOME OF THE OUTAGE TIME WAS DUE TO PLUGGED SPRAY HEADERS ON THE MIST ELIMINATOR.

PROBLEMS WITH LEAKING CIRCULATING PUMPS OCCURRED IN OCTOBER.

OTHER OUTAGE TIME WAS DUE TO THE FAILURE OF ESP DISTRIBUTOR BAFFLES.

11/80 SYSTEM 93.8 96.0 96.0 93.8 720 704 676

** PROBLEMS/SOLUTIONS/COMMENTS

FAILURE OF PRESCRUBBER RECIRCULATION PUMPS CAUSED OUTAGE TIME IN NOVEMBER.

12/80 SYSTEM 33.9 55.9 55.9 30.6 744 408 228

** PROBLEMS/SOLUTIONS/COMMENTS

DURING DECEMBER THE BOILER WAS OUT OF SERVICE DUE TO A SCHEDULED MAINTE-NANCE OVERHAUL FOR APPROXIMATELY 360 HOURS. START-UP OF THE FGD SYSTEM WAS DELAYED ABOUT FIVE DAYS DUE TO MATERIAL DELIVERY PROBLEMS.

1/81 SYSTEM 90.0 90.0 90.0 90.0 744 744 670

** PROBLEMS/SOLUTIONS/COMMENTS

DURING JANUARY THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS

WERE ENCOUNTERED.

2/81 SYSTEM 86.0 84.0 84.0 76.0 672 607 512

** PROBLEMS/SOLUTIONS/COMMENTS

DURING FEBRUARY OUTAGE TIME WAS DUE TO LEAKS IN THE MIST ELIMINATOR AND FAILURE OF THE PRESCRUBBER SPRAY NOZZLES.

FAILURE OF THE PRESCRUBBER SPRAY NOZZLES.

3/81 SYSTEM 95.6 95.6 95.6 95.4 744 743 710

** PROBLEMS/SOLUTIONS/COMMENTS

DURING MARCH THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED.

4/81 SYSTEM 74.0 83.0 83.0 74.0 720 643 531

** PROBLEMS/SOLUTIONS/COMMENTS

DURING APRIL SOME OUTAGE TIME WAS CAUSED BY THE REPAIRS TO THE MIST ELIMINATOR SHELL AND INTERNALS.

ADDITIONAL OUTAGE TIME WAS DUE TO THE REPLACEMENT OF THE BOOSTER BLOWER DISCHARGE DUCT EXPANSION JOINT.

5/81 SYSTEM 98.1 98.1 98.1 744 744 730

** PROBLEMS/SOLUTIONS/COMMENTS

DURING MAY REPAIRS WERE PERFORMED ON THE MIST ELIMINATOR SHELL.

6/81 SYSTEM 100.0 100.0 100.0 100.0 720 720 720

DELMARVA POWER & LIGHT: DELAWARE CITY 1 (CONT.)

_____PERFORMANCE DATA------PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS FACTOR ** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO PROBLEMS WERE ENCOUNTERED DURING JUNE. 99.2 744 744 738 99.2 99.2 99.2 7/81 SYSTEM 77.4 77.4 77.4 46.9 744 451 349 8/81 SYSTEM ** PROBLEMS/SOLUTIONS/COMMENTS EXTENSIVE REPAIRS WERE MADE TO THE VENTURI PRESCRUBBER BRICK WORK DURING A SCHEDULED AUGUST BOILER OUTAGE. 95.1 95.0 720 719 9/81 SYSTEM 95.1 95.1 684 ** PROBLEMS/SOLUTIONS/COMMENTS THE FGD SYSTEM WAS DOWN FOR PART OF SEPTEMBER FOR REPAIRS TO THE PRESCRUB-BER MIST ELIMINATOR. 10/81 SYSTEM 29.9 57.4 71.1 22.8 744 296 170 ** PROBLEMS/SOLUTIONS/COMMENTS ON OCTOBER 1 THE UNIT WAS SHUTDOWN FOR AN OVERHAUL. 11/81 SYSTEM 70.1 70.1 70.1 70.1 720 720 505 ** PROBLEMS/SOLUTIONS/COMMENTS DURING OCTOBER AND NOVEMBER CONTINUAL PROBLEMS WERE ENCOUNTERED WITH THE PRESCRUBBER CIRCULATING PUMPS. THIS PROBLEM RESULTED FROM PUMP PLUGGING RELATED TO INADEQUATE SCRUBBING OF THE GAS. THIS ULTIMATELY WAS THE RESULT OF AN INSUFFICIENT NUMBER OF PUMPS. 12/81 SYSTEM 72.6 67.6 68.4 59.4 744 654 442 ** PROBLEMS/SOLUTIONS/COMMENTS OUTAGE TIME FOR THE BOILER DURING DECEMBER WAS DUE TO SUPERHEATER TUBE IFAKS. CONTINUED PROBLEMS WITH THE PRESATURATOR CIRCULATING PUMPS AND PLUGGING OF THE PRESATURATOR AND ESP'S CAUSED THE SYSTEM UNAVAILABLE TIME. 1/82 SYSTEM 68.5 69.4 69.5 735 510 ** PROBLEMS/SOLUTIONS/COMMENTS DURING JANUARY THE SYSTEM WAS OFF-LINE PART OF THE MONTH DUE TO NECESSARY CLEANING OF THE MODULES AND TO REPLACE THE PRESATURATOR NOZZLE. 2/82 SYSTEM 91.5 91.5 91.5 91.5 672 672 615 ** PROBLEMS/SOLUTIONS/COMMENTS DURING JAHUARY AND FEBRUARY LEAKS IN THE PRESATURATOR PIPING ACCOUNTED FOR SOME OF THE DOWN TIME. PURGE LINE PLUGGING CAUSED ADDITIONAL OUTAGE TIME IN FEBRUARY.

64.9

64.9

744

744

483

3/82 SYSTEM

64.9

64.9

DELMARVA POWER & LIGHT: DELAWARE CITY 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS FACTOR ** PROBLEMS/SOLUTIONS/COMMENTS PROBLEMS WERE ENCOUNTERED WITH THE REGENERATING SECTION OF THE SYSTEM DURING MARCH. 4/82 SYSTEM 100.0 100.0 100.0 100.0 720 720 720 5/82 SYSTEM 92.2 92.2 92.2 92.2 744 744 686 ** PROBLEMS/SOLUTIONS/COMMENTS DURING APRIL AND MAY NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED. 6/82 SYSTEM 82.5 82.5 82.5 82.5 720 594 720 ** PROBLEMS/SOLUTIONS/COMMENTS DURING JUNE THE SYSTEM WAS SHUT DOWN PART OF THE TIME TO REPAIR THE BRICK LINING IN THE PRESATURATOR. 7/82 SYSTEM 63.8 63.8 63.8 744 744 475 63.8 ** PROBLEMS/SOLUTIONS/COMMENTS OUTAGE TIME OCCURRED DURING JULY DUE TO A HIGH PRESSURE DROP IN THE PRESATURATOR. THE DROP WAS CAUSED BY COKE CARRYOVER TO THE ESP SEAL POTS. EVAPORATOR PROBLEMS ACCOUNTED FOR AN OUTAGE DURING THE MONTH. 8/82 SYSTEM 90.2 90.2 90.2 90.2 744 744 671 ** PROBLEMS/SOLUTIONS/COMMENTS PART OF THE OUTAGE TIME DURING AUGUST WAS DUE TO LEAKS IN THE PRESATURATOR CIRCULATION PIPING. FAILURE OF THE PRESATURATOR SPRAY NOZZLE TIP ALSO RESULTED IN DOWN TIME DURING THE MONTH.

28.3 ** PROBLEMS/SOLUTIONS/COMMENTS

77.3

9/82 SYSTEM

THE UNIT WAS DOWN DURING PART OF SEPTEMBER FOR AN ANNUAL INSPECTION.

28.3

LEAKS IN THE PRESATURATOR RECIRCULATION PIPING CREATED DOWN TIME FOR THE FGD SYSTEM IN SEPTEMBER.

720

264

204

ADDITIONAL OUTAGE TIME RESULTED FROM LEAKS IN THE DUCTWORK EXPANSION JOINTS.

AN OUTAGE OCCURRED DURING SEPTEMBER FOR COKE SLAG BURN OUT.

10/82 SYSTEM 98.9 98.9 98.9 98.9 744 736 744

77.3

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING OCTOBER.

11/82 SYSTEM 97.9 97.9 97.9 97.9 720 720 705

DELMARVA POWER & LIGHT: DELAWARE CITY 1 (CONT.)

------PERFORMANCE DATA------PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAD SO2 PART. HOURS HOURS FACTOR 

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE REPORTED BY THE UTILITY DURING NOVEMBER.

81.6

81.6

12/82 SYSTEM

81.6

744 744 607

** PROBLEMS/SOLUTIONS/COMMENTS

DURING DECEMBER THE UNIT WAS DOWN FOR 45 HOURS TO CLEAN PLUGGED SCREENS ON THE PRESATURATOR CIRCULATION PUMPS.

THE REMAINDER OF DOWN TIME DURING THE MONTH WAS DUE TO PROBLEMS WITH THE ACID PLANTS.

1/83 SYSTEM 89.9 74.7 74.7 74.7 744 744 556

81.6

** PROBLEMS/SOLUTIONS/COMMENTS

OUTAGE TIME OCCURRED DURING JANUARY DUE TO THE BALANCING OF A BOOSTER FAN.

THE CLEANING OF A SUCTION SCREEN ON THE PRESATURATOR PRODUCED ADDITIONAL OUTAGE TIME IN JANUARY.

THE UNIT WAS DOWN DURING JANUARY TO PERMIT REPAIR WORK ON THE ACID PLANT.

2/83 SYSTEM 97.3 69.3 69.3 69.3 672 672 466

** PROBLEMS/SOLUTIONS/COMMENTS

REPAIR WORK ON THE ESP CAUSED AN OUTAGE DURING FEBRUARY.

THE UNIT WAS DOWN DURING FEBRUARY TO PERMIT REPAIR WORK ON THE ACID PLANT TAIL GAS LINE.

3/83 SYSTEM 95.6 95 6 95.6 95.6 744 744 711

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING MARCH.

4/83 SYSTEM 94.7 94.7 94.7 94.7 720 720 682 5/83 SYSTEM 98.9 98.9 98.9 98.91 744 744 736

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING APRIL AND MAY.

6/83 SYSTEM 84.7 84.7 84.7 84.7 720 720 610

** PROBLEMS/SOLUTIONS/COMMENTS

REPAIRS ON THE BRICK LINING IN THE PRESATURATOR CAUSED A FORCED OUTAGE DURING JUNE.

7/83 SYSTEM 100.0 100.0 100.0 100.0

744 744 744 8/83 SYSTEM 96.0 96.0 100.0 96.0 744 744 714 PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED

DURING JULY AND AUGUST.

9/83 SYSTEM 71.3 92.8 92.8 71.3 720 553 513

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS SHUT DOWN ON SEPTEMBER 24 FOR AN ANNUAL INSPECTION AND MAINTENANCE.

10/83 SYSTEM 50.7 86.9 86.9 50.7 744 434 377

** PROBLEMS/SOLUTIONS/COMMENTS

UNIT 1 WAS OUT OF SERVICE FROM SEPTEMBER 24 TO OCTOBER 14, 1983 FOR A SCHEDULED OUTAGE. DURING THIS PERIOD AN ANNUAL BOILER INSPECTION AND FGD SYSTEM MAINTENANCE WAS CONDUCTED.

THE FGD SYSTEM WAS DOWN DURING PART OF OCTOBER DUE TO A LACK OF SODIUM SULFITE ABSORBING SOLUTION.

11/83 SYSTEM 94.2 94.2 94.2 94.2 720 720 678

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURING NOVEMBER.

12/83 SYSTEM 82.8 82.8 82.8 82.8 744 744 616

** PROBLEMS/SOLUTIONS/COMMENTS

FGD SYSTEM OUTAGE TIME DURING DECEMBER WAS DUE IN PART TO EXTREME COLD WEATHER CONDITIONS.

BRIEF OUTAGES OCCURRED DURING THE MONTH DUE TO MIST ELIMINATOR LEAKS.

1/84 SYSTEM 98.9 98.9 98.9 744 744 736

** PROBLEMS/SOLUTIONS/COMMENTS

A LACK OF ABSORBING SOLUTION DUE TO EVAPORATOR CIRCULATING PUMP PROBLEMS AND PLUGGED EVAPORATOR SOLUTION HEADERS LIMITED THE BURNING OF HIGH SULFUR COKE DURING JANUARY.

2/84 SYSTEM 84.5 84.5 84.5 696 696 588

** PROBLEMS/SOLUTIONS/COMMENTS

PRESATURATOR CLEANING CONTRIBUTED TO OUTAGE TIME DURING FEBRUARY.

THE UTILITY REPORTED REPLACING FALLEN ACID BRICK DURING FEBRUARY.

MIST ELIMINATOR REPAIRS ACCOUNTED FOR ADDITIONAL DOWN TIME DURING THE MONTH.

PRESATURATOR RECIRCULATING PROBLEMS WERE REPORTED DURING FEBRUARY.

3/84 SYSTEM 98.4 744 744 732 98.4 98.4 98.4 4/84 SYSTEM 99.6 99.6 99.6 99.6 720 720 717 5/84 SYSTEM 97.2 97.2 97.2 97.2 744 744 703

DELMARVA POWER & LIGHT: DELAWARE CITY 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

#### ** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE REPORTED DURING MARCH THROUGH MAY.

6/84	SYSTEM	720
7/84	SYSTEM	744
8/84	SYSTEM	744
9/84	SYSTEM	720

#### ** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE PERIOD OF JUNE THROUGH SEPTEMBER 1984.

# SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

		051MABUA 00UED	A LYOUT
COMPANY NAME		DELMARVA POWER	& LIGHT
PLANT NAME		DELAWARE CITY	
UNIT NUMBER		2	
CITY		DELAWARE CITY	
STATE		DELAWARE	
REGULATORY CLASSI		E	
PARTICULATE EMISS	L\DM - MOITATIMIL HOIS	129.	( .300 LB/MMBTU)
SO2 EMISSION LIMI	TATION - NG/J	*****	(**** LB/MMBTU)
NOX EMISSION LIMI	L\DN - NOITAT: L\DN - NOITAT:	*****	(***** LB/MMBTU) (***** LB/MMBTU)
	ING CAPACITY - MW	180	
	TING CAPACITY - MW	180 60	
	NG CAPACITY W/FGD - MW	495	
	ING CAPACITY WO/FGD - MW	495	
	BED CAPACITY - MW	60	
Edoliveril compet	The service of the se	30	
** INTT DATA - B	BOILER AND STACK		
BOILER SUPPL		RILEY STOKER	
BOILER TYPE	:1ER	PULVERIZED COA	•
BOILER SERVI	CE LOAD	BASE	<b>-</b>
			( 407444 1074)
	R FLUE GAS FLOW - CU.M/S	139.21	( 295000 ACFM)
	GAS TEMPERATURE - C	215.6 152.	( 420 F)
STACK HEIGHT			( 500 FT)
STACK SHELL		CONCRETE	
STACK TOP DI	IAMETER - M	6.1	( 20.0 FT)
** FUEL DATA			
FUEL TYPE		COKE	
FUEL GRADE		BITUMINOUS	
	CONTENT - J/G	32564.	( 14000 BTU/LB)
	CONTENT - BTU/LB		13500-14500
AVERAGE ASH	CONTENT - X	.50	
RANGE ASH CO	NTENT - X	0.3-0.7	
AVERAGE MOIS	STURE CONTENT - %	.70	
RANGE MOISTL	JRE CONTENT - X	0.5-1.2	
AVERAGE SULF	FUR CONTENT - %	7.00	
	CONTENT - %	5.0-8.0	
AVERAGE CHLC	ORIDE CONTENT - %	*****	
RANGE CHLORI	IDE CONTENT - %	*****	
*** PARTICLE CONT	rol		
** MECHANICAL CO	LLECTOR		
NUMBER		3	
TYPE		TUBULAR	
SUPPLIER		PRAT-DANIEL	
PARTICLE REM	10VAL EFFICENCY -%	92.0	
** FABRIC FILTER	₹		
NUMBER		0	
TYPE		NONE	
TYPICAL GAS/	CLOTH RATIO - M/MIN	.6	( 2.0 FT/MIN)
** ESP			
NUMBER		3	
TYPE		COLD SIDE	
SUPPLIER		WESTERN PREC.	DIVISION, JOY
	GAS CAPACITY - CU.M/S	34.8	( 73700 ACFM)
	GAS TEMPERATURE - C	54.4	( 130 F)
PRESSURE DRO		.2	( 1. IN-H2O)
	10VAL EFFICENCY - %	95.0	· · · · · · · · · · · · · · · · · · ·
TON FAULE REF	TOTAL ELIZABITOT A	,5.4	
** PARTICLE SCRU	IBBER		
NUMBER	, out the same of	3	
INITIAL STAR	T_IID DATE	4/80	
		VENTURI TOWER	
GENERIC TYPE			T/ROTTOM_ENTRY DILMO DOD
SPECIFIC TYP			T/BOTTOM-ENTRY PLUMB BOB
TRADE NAME/C	JUUUN NAUE	N/A	
SUPPLIER		AIRPOL	
DIMENSIONS -	, F1	20 DIA X 70.0	

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DELMARVA POWER & LIGHT: DELAWARE CITY 2 (CONT.)
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CARBON STEEL
    SHELL GENERIC MATERIAL
                                               AISI 1110
    SHELL SPECIFIC MATERIAL
                                                ORGANIC; INORGANIC
    LINER GENERIC MATERIAL
                                               GLASS FLAKE-FILLED POLYESTER; PREFIRED BRICK/SHA
    LINER SPECIFIC MATERIAL
                                               NONE
    GAS CONTACTING DEVICE TYPE
    NUMBER OF CONTACTING ZONES
                                                1
                                                             ( 5000 GPM)
(50.9 GAL/1000ACF)
    LIQUID RECIRCULATION RATE - LITER/S
                                                315.0
    L/G RATIO - LITER/CU.M
                                                  6.8
                                                    ۰.5
                                                             ( 2.0 IN-H2O)
    PRESSURE DROP - KPA
                                                             ( 98300 ACFM)
( 430 F)
                                                  46.4
    INLET GAS FLOW RATE - CU.M/S
    INLET GAS TEMPERATURE - C
                                                 221.1
                                                    .0
    SO2 REMOVAL EFFICENCY - %
    PARTICLE REMOVAL EFFICIENCY - %
                                                 81.5
*** FGD SYSTEM
** GENERAL DATA
    SALEABLE PRODUCT/THROWAWAY PRODUCT
                                               SALEABLE PRODUCT
                                               WET SCRUBBING
    SO2 REMOVAL MODE
                                               WELLMAN LORD
    PROCESS TYPE
                                               DAVY MCKEE
    SYSTEM SUPPLIER
                                                DAVY MCKEE
    A-E FIRM
    DEVELOPMENT LEVEL
                                                FULL SCALE
                                               RETROFIT
    NEW/RETROFIT
    UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 90.00
    UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                  90.00
    CURRENT STATUS
                                                1
    COMMERCIAL START-UP
                                                5/80
    INITIAL START-UP
                                                5/80
    CONTRACT AWARDED
 ** DESIGN AND OPERATING PARAMETERS
    SPACE REQUIREMENTS - SQ M
                                               24280.3
                                                             ( 261360 SQ FT)
    OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                 144.0
 ** QUENCHER/PRESATURATOR
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                ND
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                NΩ
 ** ABSORBER
    NUMBER
                                                3
    NUMBER OF SPARES
                                                0
    GENERIC TYPE
                                                TRAY TOWER
                                                VALVE TRAY
    SPECIFIC TYPE
     TRADE NAME/COMMON TYPE
                                               BUBBLE CAP TRAY TOWER
     SUPPLIER
                                                DAVY MCKEE
    DIMENSIONS - FT
                                                20.0 X 20.0
    SHELL GENERIC MATERIAL
                                                INORGANIC
     SHELL SPECIFIC MATERIAL
                                                HYDRAULICALLY-BONDED CONCRETE
     SHELL MATERIAL TRADE NAME/COMMON TYPE
                                                PORTLAND CEMENT
    LINER GENERIC MATERIAL
                                                INORGANIC
    LINER SPECIFIC MATERIAL
                                                PREFIRED BRICK/SHAPES
     LINER MATERIAL TRADE NAME/COMMON TYPE
                                               NR
     GAS CONTACTING DEVICE TYPE
                                                VALVE TRAY
     NUMBER OF CONTACTING ZONES
     LIQUID RECIRCULATION RATE LITER/S
                                                             ( 400 GPM)
                                                             ( 5.5 GAL/1000 ACF)
( 73300 ACFM)
( 130 F)
     L/G RATIO - L/CU.M
                                                    .7
    INLET GAS FLOW - CU. M/S
                                                   34.59
     INLET GAS TEMPERATURE - C
                                                   54.4
     PARTICLE REMOVAL EFFICENCY - %
                                                    .0
 ** MIST ELIMINATOR
     PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                                PRIMARY COLLECTOR
    NUMBER PER SYSTEM
                                                 3
     GENERIC TYPE
                                                IMPINGEMENT
    SPECIFIC TYPE
                                                BAFFLE
     TRADE NAME/COMMON TYPE
                                                CLOSED VANE
    CONFIGURATION
                                                HORIZONTAL
    NUMBER OF STAGES
                                                    1
    NUMBER OF PASSES PER STAGE
                                                    1
    FREEBOARD DISTANCE - M
                                                    1.83
                                                              ( 6.0 FT)
```

#### DELMARVA POWER & LIGHT: DELAWARE CITY 2 (CONT.)

```
DISTANCE BETWEEN STAGES - CM
                                                   19.05
                                                               ( 7.5 IN)
    PRESSURE DROP - KPA
                                                               ( .3 IN-H20)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                ORGANIC
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                POLYPHENYLENE
                                                COOLED CONDENSATE
    WASH WATER SOURCE
    WASH FREQUENCY
                                                INTERMITTENT
    WASH RATE - L/S
                                                    3.2
                                                               (
                                                                  50 GAL/MIN)
** REHEATER
    NUMBER
    GENERIC TYPE
                                                DIRECT COMBUSTION
    SPECIFIC TYPE
                                                EXTERNAL COMBUSTION CHAMBER
    TRADE NAME/COMMON TYPE
                                                NATURAL GAS
    TEMPERATURE INCREASE - C
                                                  27.8
                                                                   50 F)
                                                               ſ
    INLET FLUE GAS FLOW RATE - CU. M/S
                                                  108.54
                                                               ( 230000 ACFM)
    INLET FLUE GAS TEMPERATURE - C
                                                  54.4
                                                               ( 130 F)
    OUTLET FLUE GAS TEMPERATURE - C
                                                               ( 185 F)
                                                   85.0
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                NR
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                NR
** FANS
    NUMBER
                                                 3
    NUMBER OF SPARES
                                                 0
    DESIGN
                                                CENTRIFUGAL
    SUPPLIER
                                                ROBINSON
    FUNCTION
                                                BOOSTER
    APPLICATION
                                                INDUCED DRAFT
    SERVICE
                                                DRY
    FLUE GAS FLOW RATE CU.M/S
                                                 139.21
                                                               ( 295000 ACFM)
    FLUE GAS TEMPERATURE - C
                                                  215.6
                                                               ( 420 F)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                CARBON STEEL
** DAMPERS
    FUNCTION
                                                NR
    GENERIC . TYPE
                                                NR
    SPECIFIC TYPE
                                                NR
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                NR
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                ND
    LINER GENERIC MATERIAL TYPE
                                                NR
    LINER SPECIFIC MATERIAL TYPE
                                                NR
** DUCTHORK
    DIMENSIONS
                                                8.0 X 8.0
     SHELL GENERIC MATERIAL TYPE
                                               CARBON STEEL
     SHELL SPECIFIC MATERIAL TYPE
                                               AISI 1110
     LINER GENERIC MATERIAL TYPE
                                                ORGANIC
     LINER SPECIFIC MATERIAL TYPE
                                                FIBER-REINFORCED POLYESTER
** REAGENT PREPARATION EQUIPMENT
    FUNCTION
                                                MIX TANK
    DEVICE
                                                N/A
    DEVICE TYPE
                                                AGITATED TANK
** TANKS
                                                NUMBER
    SERVICE
    -----
                                                -----
    ΝR
                                                ****
** PUMPS
    SERVICE
                                                NUMBER
                                                -----
    ABSORBER RECIRCULATION
                                                ****
** SOLIDS CONCENTRATING/DEWATERING
                                                NONE
    DEVICE
*** SALEABLE BYPRODUCTS
                                                SULFURIC ACID
                                                               ( 12.50 TPH)
    FULL LOAD QUANTITY - M T/H
                                                   11.34
```

DELMARVA POWER & LIGHT: DELAWARE CITY 2 (CONT.)

QUALITY - % 93.0
DISPOSITION MARKETED

*** SLUDGE

** TREATMENT

METHOD N/A
DEVICE N/A
PROPRIETARY PROCESS N/A

** DISFOSAL

NATURE FINAL TYPE POND

SITE TREATMENT CLAY LINING

** PROCESS CONTROL AND INSTRUMENTATION

CHEMICAL PARAMETERS PH, SOLIDS, SP.G., CONC.
MONITOR LOCATION GAS OUTLET, SOLUTION OUTLET
PROCESS CONTROL MANNER AUTOMATIC
PROCESS CHEMISTRY MODE FEEDBACK

** WATER BALANCE

WATER LOOP TYPE CLOSED

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

5/80 SYSTEM 100.0 100.0 100.0 32.3 744 240 240

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM BEGAN INITIAL AND COMMERCIAL OPERATIONS ON MAY 22, 1980. NO MAJOR PROBLEMS WERE ENCOUNTERED DURING STARTUP OR THROUGH THE REST OF THE MONTH.

6/80 SYSTEM 80.4 80.4 80.4 720 720 579

** PROBLEMS/SOLUTIONS/COMMENTS

THE CHEVRON PACKING IN THE MIST ELIMINATOR FAILED CAUSING SOME FGD SYSTEM OUTAGE TIME DURING JUNE.

FAILURE OF THE CIRCULATION PUMPS ALSO CAUSED OUTAGE TIME DURING THE MONTH.

7/80 SYSTEM 50.1 50.1 50.1 50.1 744 744 373

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS DOWN FOR PART OF THE MONTH TO REPAIR A LEAK IN THE MIST ELIMINATOR. IT WAS ALSO DOWN TO REBUILD THE CHEVRON PACKING.

8/80 SYSTEM 92.9 92.9 92.9 744 744 691

** PROBLEMS/SOLUTIONS/COMMENTS

REPAIRS WERE MADE TO THE ESP DURING AUGUST.

9/80 SYSTEM 78.2 78.2 78.2 78.2 720 720 563

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS OFF LINE DURING SEPTEMBER DUE TO NECESSARY REPAIR OF THE CIRCULATING PUMPS AND THE MIST ELIMINATOR.

FGD SYSTEM OUTAGE TIME OCCURRED DUE TO INLET DUCT EXPANSION JOINT REPAIRS.

DELMARVA POWER & LIGHT: DELAWARE CITY 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

10/80 SYSTEM 60.0 60.0 60.0 744 743 445

** PROBLEMS/SOLUTIONS/COMMENTS

DURING OCTOBER THE MAJORITY OF DOWN TIME WAS DUE TO THE ACID PLANT BEING DOWN. IT WAS UNABLE TO PROCESS SO2 FROM THE WELLMAN LORD SOLUTION REGENERATION SECTION.

11/80 SYSTEM 98.3 98.3 98.3 720 720 708

** PROBLEMS/SOLUTIONS/COMMENTS

DURING NOVEMBER OUTAGE TIME WAS REQUIRED TO REPAIR LEAKS IN THE PRE-SCRUBBER.

12/80 SYSTEM 100.0 100.0 100.0 100.0 744 744 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED NO FGD-RELATED PROBLEMS DURING THE MONTH OF DECEMBER.

1/81 SYSTEM 93.0 93.0 93.0 93.0 744 744 692 2/81 SYSTEM 96.0 96.0 96.0 96.0 672 672 648

** PROBLEMS/SOLUTIONS/COMMENTS

DURING JANUARY AND FEBRUARY THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED.

.5

PROBLEMS WERE ENCOUNTERED

3/81 SYSTEM 57.5 89.0 89.0 57.5 744 481 428

** PROBLEMS/SOLUTIONS/COMMENTS

DURING MARCH THE BOILER WAS OUT OF SERVICE FOR PART OF THE MONTH DUE TO AN OVERHAUL.

REPAIRS TO A LEAK IN THE MIST ELIMINATOR CAUSED SOME OUTAGE TIME.

4/81 SYSTEM 64.0 84.0 84.0 64.0 720 553 464

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER WAS OUT OF SERVICE APPROXIMATELY 167 HOURS DURING APRIL DUE TO A SCHEDULED MAINTENANCE OUTAGE.

THE FGD SYSTEM WAS UNAVAILABLE APPROXIMATELY 256 HOURS DUE TO THE REPLACEMENT OF THE PRESATURATOR MIST ELIMINATOR INTERNALS AND THE BRICK LINING.

5/81 SYSTEM 97.5 97.5 97.5 744 744 726

** PROBLEMS/SOLUTIONS/COMMENTS

DURING MAY REPAIRS WERE PERFORMED ON THE BOOSTER BLOWER INSPECTION DOOR.

6/81 SYSTEM 75.8 75.8 75.8 75.8 720 720 546

** PROBLEMS/SOLUTIONS/COMMENTS

ON JUNE 23 THE SYSTEM WAS SHUT DOWN DUE TO A HIGH PRESSURE DROP. ON INSPECTION, IT WAS DESCOVERED THAT THE PRESATURATOR NOZZLE HAD FAILED, THERE WAS A CONSIDERABLE COKE BUILDUP IN THE PRESATURATOR MIST ELIMINATOR BOX, THE MIST ELIMINATOR CHEVRONS HAD FAILED, THERE WAS A LARGE COKE BUILDUP IN THE

DELMARVA POWER & LIGHT: DELAWARE CITY 2 (CONT.)

.----PERFORMANCE DATA-----PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD SO2 PART. HOURS HOURS FACTOR ESP INLET SEAL POT AND A HIGH SOLIDS BUILDUP IN THE BOTTOM OF THE SO2 ABSORBER. REPAIRS CONSISTED OF REPLACING THE PRESATURATOR NOZZLE TIP AND CLEANING THE BUILDUP. 76.9 76.9 76.9 76.9 744 744 572 7/81 SYSTEM ** PROBLEMS/SOLUTIONS/COMMENTS DURING JULY, THE ACID BRICK LINING ON THE INLET TO THE PRESCRUBBER FAILED. IN ADDITION, PROBLEMS WERE ENCOUNTERED WITH THE PRESCRUBBER NOZZLE TIP. 8/81 SYSTEM 97.8 97.8 97.8 97.8 744 744 728 720 9/81 SYSTEM 99.2 96.3 96.3 86.7 648 624 ** PROBLEMS/SOLUTIONS/COMMENTS DURING SEPTEMBER, THE BOILER WAS OFF LINE FOR 72 HOURS TO REPAIR A SUPER-HEATER TUBE LEAK. 10/81 SYSTEM 100.0 100.0 100.0 100.0 744 744 744 11/81 SYSTEM 89.2 89.2 89.2 89.2 720 720 642 ** PROBLEMS/SOLUTIONS/COMMENTS DURING NOVEMBER THE FGD SYSTEM WAS DOWN 62 HOURS TO CLEAN THE ESP SEAL POT AND TO REPLACE THE TIP OF A PRESATURATOR SPRAY NOZZLE. 12/81 SYSTEM 98.9 98.9 98.9 98.9 744 744 736 ** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING DECEMBER. 1/82 SYSTEM 78.5 78.5 78.5 78.5 744 744 584 ** PROBLEMS/SOLUTIONS/COMMENTS SOME OF THE OUTAGE TIME IN JANUARY WAS DUE TO A STEAM SHORTAGE. 2/82 SYSTEM 79.7 79.7 79.7 79.7 536 672 672 ** PROBLEMS/SOLUTIONS/COMMENTS SOME OF THE OUTAGE TIME IN JANUARY AND FEBRUARY WAS DUE TO THE REPLACEMENT OF A BOOSTER BLOWER BEARING. THE SYSTEM WAS OFF-LINE PART OF THE MONTH TO REPAIR A PRESATURATOR CIRCULATING PUMP. OUTAGE TIME WAS NECESSARY TO UNPLUG THE PURGE LINE IN FEBRUARY. 3/82 SYSTEM 46.4 75.3 75.3 46.4 744 458 345 ** PROBLEMS/SOLUTIONS/COMMENTS

513 502

97.8

SCRUBBING SOLUTION SECTION.

97.8

HAUL.

69.7

4/82 SYSTEM

DURING MARCH THE BOILER WAS OFF-LINE PART OF THE TIME FOR THE ANNUAL OVER-

720

THE SYSTEM WAS UNAVAILABLE PART OF THE MONTH DUE TO PROBLEMS WITH THE

69.7

PERIOD	MODULE	AVAILABILIT	TY OPERABILITY	RELIABILITY	UTILIZATION				FGD CAP.
	** PROE	BLEMS/SOLUT	IONS/COMMENTS						
			THE BOILER WAS		URING APRIL	DUE TO THE	ANNUAL (	OVERHAU	L WHICH
5/82	SYSTEM	96.0	96.0	96.0	96.0		744	744	714
	** PRO	BLEMS/SOLUT	IONS/COMMENTS						
			THE UTILITY R DURING MAY.	EPORTED THAT	NO MAJOR FG	D-RELATED F	ROBLEMS	WERE E	NCOUNTERED
6/82	SYSTEM	96.6	96.6	96.6	96.6		720	720	696
	** PRO	BLEMS/SOLUT	IONS/COMMENTS						
			THE UTILITY R DURING JUNE.	EPORTED THAT	NO MAJOR FG	D-RELATED F	ROBLEMS	WERE E	XPERIENCED
7/82	SYSTEM	89.9	89.9	89.9	89.9		744	744	669
	** PRO	BLEMS/SOLUT	IONS/COMMENTS						
			A LACK OF SOL DURING JULY.	UTION DUE TO	EVAPORATOR	PROBLEMS AC	COUNTED	FOR OU	TAGE TIME
8/82	SYSTEM	94.2	95.0	95.0	94.2		744	<b>7</b> 38	701
	** PRO	BLEMS/SOLUT	IONS/COMMENTS						
			NO MAJOR FGD- DURING AUGUST		LEMS WERE EN	ICOUNTERED E	SY THE U	TILITY	
9/82	SYSTEM	93.9	93.9	93.9	93.9		720	720	676
	** PRO	BLEMS/SOLUT	IONS/COMMENTS						
			THE UTILITY R		NO MAJOR FG	D-RELATED F	ROBLEMS	WERE E	NCOUNTERED
10/82	SYSTEM	98.4	98.4	98.4	98.4		744	744	732
11/82	SYSTEM	97.2	97.2	97.2	97.2		720	720	700
12/82	SYSTEM	97.7	97.7	97.7	97.7		744	744	727
	** PRO	BLEMS/SOLUT	IONS/COMMENTS						
			THE UTILITY R				ROBLEMS	WERE E	NCOUNTERED
1/83	SYSTEM	98.7	98.7	98.7	98.7		744	744	734
	** PRO!	BLEMS/SOLUT	IONS/COMMENTS						
			THE UTILITY R		NO MAJOR FG	SD-RELATED I	PROBLEMS	WERE E	NCOUNTERED

2/83 SYSTEM 97.5 97.5 97.5 672 672 655

DURING JANUARY.

DELMARVA POWER & LIGHT: DELAWARE CITY 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE REPORTED BY THE UTILITY DURING FEBRUARY.

3/83 SYSTEM 32.0 88.8 88.8 32.0 744 268 238

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER WAS DOWN FROM MARCH 12 TO MARCH 31 FOR AN ANNUAL OUTAGE.

4/83 SYSTEM 96.8 96.8 96.8 96.8 720 720 697

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING APRIL.

5/83 SYSTEM 91.7 91.7 91.7 91.7 744 744 682

** PROBLEMS/SOLUTIONS/COMMENTS

REPAIRS TO THE ESP CAUSED A FORCED OUTAGE DURING MAY.

BOOSTER FAN REPAIRS ALSO CAUSED DOWN TIME DURING THE MONTH.

6/83 SYSTEM 81.0 81.0 81.0 81.0 720 720 583

** PROBLEMS/SOLUTIONS/COMMENTS

DOWN TIME OCCURRED DURING JUNE DUE TO REPAIRS ON A BOOSTER FAN.

REPAIRS ON A PRESATURATOR SPRAY NOZZLE ALSO FORCED THE SYSTEM OUT OF SERVICE DURING PART OF JUNE.

7/83 SYSTEM 86.6 86.6 86.6 86.6 744 744 644

** PROBLEMS/SOLUTIONS/COMMENTS

UNIT 2 WAS DOWN DURING PART OF JULY TO REMOVE A SOLIDS BUILD UP IN THE PRE-SCRUBBER AND PRESCRUBBER INLET DUCT. SOME PRESCRUBBER SPRAY NOZZLES WERE REPLACED DURING THIS PERIOD.

BOOSTER FAN REPAIRS WERE MADE AT UNIT 2 DURING JULY.

8/83 SYSTEM 98.0 98.0 100.0 98.0 744 744 729

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING AUGUST.

9/83 SYSTEM 81.8 81.8 81.8 720 720 589

** PROBLEMS/SOLUTIONS/COMMENTS

UNIT 2 WAS DOWN DURING PART OF SEPTEMBER TO REPAIR BRICKWORK AT THE INLET TO THE FRESCRUBBER AND TO CLEAN THE PRESCRUBBER.

THE UNIT WAS DOWN DURING PART OF THE MONTH TO CLEAN THE ESP INLET SEAL POTS.

10/83 SYSTEM 98.7 98.7 98.7 98.7 744 744 734

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

_____

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURING OCTOBER.

11/83 SYSTEM 82.2 82.2 82.2 82.2 720 720 592

** PROBLEMS/SOLUTIONS/COMMENTS

PRESCRUBBER SPRAY NOZZLES WERE REPLACED DURING NOVEMBER.

MIST ELIMINATOR LEAKS WERE REPAIRED DURING NOVEMBER.

THE PRESCRUBBER WAS CLEANED DURING THE MONTH CONTRIBUTING TO FGD SYSTEM DOWN TIME.

12/83 SYSTEM 92.2 92.2 92.2 744 744 686

** PROBLEMS/SOLUTIONS/COMMENTS

MIST ELIMINATOR LEAKS RESULTED IN FGD SYSTEM OUTAGES DURING THE MONTH.

LEAKS IN THE PRESCRUBBER CIRCULATION PIPING ALSO CONTRIBUTED TO DOWN TIME DURING DECEMBER.

1/84 SYSTEM 81.7 81.7 81.7 744 744 608

** PROBLEMS/SÖLUTIONS/COMMENTS

A LACK OF ABSORBING SOLUTION DUE TO EVAPORATOR CIRCULATING PUMP PROBLEMS AND PLUGGED EVAPORATOR SOLUTION HEADERS LIMITED THE BURNING OF HIGH SULFUR COKE DURING JANUARY.

THE UTILITY REPORTED THAT BOOSTER FAN REPAIRS WERE MADE DURING JANUARY.

THE REPAIR OF BROKEN WIRES IN THE ESP'S RESULTED IN OUTAGE TIME DURING THE MONTH.

THE FAILURE OF PRESATURATOR CIRCULATING PUMPS ACCOUNTED FOR ADDITIONAL DOWN TIME DURING JANUARY.

THE REMOVAL OF COKE BUILD UP IN THE ESP'S CONTRIBUTED TO FGD SYSTEM DOWN TIME DURING THE MONTH.

2/84 SYSTEM 93.8 93.8 93.8 93.8 696 696 653 3/84 SYSTEM 96.4 96.4 96.4 96.4 744 744 717 4/84 SYSTEM 98.2 98.2 98.2 98.2 720 720 707

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE REPORTED DURING FEBRUARY THROUGH APRIL.

5/84 SYSTEM 23.1 53.1 56.1 21.0 744 294 156

** PROBLEMS/SOLUTIONS/COMMENTS

THE ABSORBER WAS DOWN FOR MAINTENANCE DURING THE ANNUAL BOILER OUTAGE IN MAY.

PROBLEMS WITH PLUGGING OF THE PRESATURATOR WERE REPORTED DURING MAY.

6/84 SYSTEM 720

DELMARVA POWER & LIGHT: DELAWARE CITY 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL SO2 PART. HOURS HOURS FACTOR

7/84 SYSTEM

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE PERIOD OF JUNE THROUGH SEPTEMBER 1984.

# SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

DELMARVA POWER & LIGHT COMPANY NAME DELAWARE CITY PLANT NAME UNIT NUMBER DELAWARE CITY CTTY DELAWARE STATE REGULATORY CLASSIFICATION Ε PARTICULATE EMISSION LIMITATION - NG/J 129. ( .300 LB/MMBTU)
****** (****** LB/MMBTU)
****** (****** LB/MMBTU) SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J ***** NET PLANT GENERATING CAPACITY - MW 180 GROSS UNIT GENERATING CAPACITY - MW 60 NET UNIT GENERATING CAPACITY W/FGD - MW NET UNIT GENERATING CAPACITY WO/FGD - MW 495 495 EQUIVALENT SCRUBBED CAPACITY - MW ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER RILEY STOKER BOILER TYPE PULVERIZED COAL BASE BOILER SERVICE LOAD 139.21 ( 295000 ACFM)
215.6 ( 420 F)
152. ( 500 FT)
CONCRETE
6.1 ( 20.0 FT) DESIGN BOILER FLUE GAS FLOW - CU.M/S BOILER FLUE GAS TEMPERATURE - C STACK HEIGHT - M STACK SHELL STACK TOP DIAMETER - M 6.1 ( 20.0 FT) ** FUEL DATA FUEL TYPE COKE FUEL GRADE BITUMINOUS AVERAGE HEAT CONTENT - J/G 32564. ( 14000 BTU/LB) RANGE HEAT CONTENT - BTU/LB 13500-14500 AVERAGE ASH CONTENT - % .50 RANGE ASH CONTENT - % 0.3-0.7 .70 .9 AVERAGE MOISTURE CONTENT - % RANGE MOISTURE CONTENT - % 0.5-1.2 AVERAGE SULFUR CONTENT - % 7.00 RANGE SULFUR CONTENT - % 5.0-8.0 AVERAGE CHLORIDE CONTENT - % ***** RANGE CHLORIDE CONTENT - X ***** *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER TYPE TUBULAR PRAT-DANIEL SUPPLIER. PARTICLE REMOVAL EFFICENCY -% 92.0 ** FABRIC FILTER NUMBER ß NONE .6 ( 2.0 FT/MIN) TYPICAL GAS/CLOTH RATIO - M/MIN ** ESP NUMBER TYPE COLD SIDE WESTERN PREC. DIVISION, JOY SUPPLIER 34.8 ( 73700 ACFM) 54.4 ( 130 F) .2 ( 1. IN-H20) INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE - C FRESSURE DROP - KPA PARTICLE REMOVAL EFFICENCY - % 95.0 ** PARTICLE SCRUBBER NUMBER INITIAL START-UP DATE 4/80 VENTURI TOWER GENERIC TYPE VARIABLE-THROAT/BOTTOM-ENTRY PLUMB BOB SPECIFIC TYPE TRADE NAME/COMMON NAME AIRPOL SUPPLIER DIMENSIONS FT 20 DIA X 70.0

DELMARVA POWER & LIGHT: DELAWARE CITY 3 (CONT.)

```
CARBON STEEL
    SHELL GENERIC MATERIAL
    SHELL SPECIFIC MATERIAL
                                               AISI 1110
                                               ORGANIC; INORGANIC
    LINER GENERIC MATERIAL
    LINER SPECIFIC MATERIAL
                                               GLASS FLAKE-FILLED POLYESTER; PREFIRED BRICK/SHA
    GAS CONTACTING DEVICE TYPE
                                               NONE
    NUMBER OF CONTACTING ZONES
                                                1
                                                315.0
    LIQUID RECIRCULATION RATE - LITER/S
                                                             ( 5000 GPM)
                                                 6.8
                                                              (50.9 GAL/1000ACF)
     L/G RATIO - LITER/CU.M
    PRESSURE DROP - KPA
                                                    . 5
                                                              ( 2.0 IN-H20)
                                                             ( 98300 ACFM)
( 430 F)
    INLET GAS FLOW RATE - CU.M/S
                                                  46.4
    INLET GAS TEMPERATURE - C
                                                 221.1
     SO2 REMOVAL EFFICENCY - %
                                                    . 0
    PARTICLE REMOVAL EFFICIENCY - %
                                                  81.5
*** FGD SYSTEM
 ** GENERAL DATA
    SALEABLE PRODUCT/THROWAWAY PRODUCT
                                               SALEABLE PRODUCT
                                               WET SCRUBBING
     SO2 REMOVAL MODE
     PROCESS TYPE
                                               WELLMAN LORD
    SYSTEM SUPPLIER
                                               DAVY MCKEE
                                               DAVY MCKEE
     A-E FIRM
    DEVELOPMENT LEVEL
                                               FULL SCALE
                                               RETROFIT
    NEW/RETROFIT
    UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 90.00
    UNIT DESIGN SO2 REMOVAL EFFICIENCY - X
                                                  90.00
    CURRENT STATUS
                                                1
     COMMERCIAL START-UP
                                                5/80
    INITIAL START-UP
                                                5/80
    CONTRACT AWARDED
                                                9/77
 ** DESIGN AND OPERATING PARAMETERS
    SPACE REQUIREMENTS - SQ M
                                                             ( 261360 SQ FT)
                                               24280.3
     OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                144.0
 ** QUENCHER/PRESATURATOR
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               ND
     CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               ND
 ** ABSORBER
    NUMBER
                                                3
    NUMBER OF SPARES
                                                0
    GENERIC TYPE
                                               TRAY TOWER
    SPECIFIC TYPE
                                               VALVE TRAY
    TRADE NAME/COMMON TYPE
                                               BUBBLE CAP TRAY TOWER
    SUPPLIER
                                               DAVY MCKEE
     DIMENSIONS - FT
                                               20.0 X 20.0
     SHELL GENERIC MATERIAL
                                               INORGANIC
     SHELL SPECIFIC MATERIAL
                                               HYDRAULICALLY-BONDED CONCRETE
     SHELL MATERIAL TRADE NAME/COMMON TYPE
                                               PORTLAND CEMENT
     LINER GENERIC MATERIAL
                                               INORGANIC
     LINER SPECIFIC MATERIAL
                                               PREFIRED BRICK/SHAPES
     LINER MATERIAL TRADE NAME/COMMON TYPE
                                               ИR
     GAS CONTACTING DEVICE TYPE
                                               VALVE TRAY
    NUMBER OF CONTACTING ZONES
    LIQUID RECIRCULATION RATE - LITER/S
                                                  25.
                                                              ( 400 GPM)
    L/G RATIO L/CU.M
                                                   .7
                                                              ( 5.5 GAL/1000 ACF)
    INLET GAS FLOW - CU. M/S
                                                  34.59
                                                             ( 73300 ACFM)
    INLET GAS TEMPERATURE - C
                                                  54.4
                                                             ( 130 F)
    PARTICLE REMOVAL EFFICENCY - %
                                                    . 0
 ** MIST ELIMINATOR
    PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                               PRIMARY COLLECTOR
    NUMBER PER SYSTEM
                                                3
    GENERIC TYPE
                                               IMPINGEMENT
    SPECIFIC TYPE
                                               BAFFLE
    TRADE NAME/COMMON TYPE
                                               CLOSED VANE
    CONFIGURATION
                                               HORIZONTAL
    NUMBER OF STAGES
                                                   1
    NUMBER OF PASSES PER STAGE
    FREEBOARD DISTANCE - M
                                                   1.83
                                                             ( 6.0 FT)
```

#### DELMARVA POWER & LIGHT: DELAWARE CITY 3 (CONT.)

```
19.05 ( 7.5 IN)
    DISTANCE BETWEEN STAGES - CM
                                                               ( .3 IN-H20)
    PRESSURE DROP - KPA
                                                    . 1
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                ORGANIC
                                                POLYPHENYLENE
    CONSTRUCTION MATERIAL SPECIFIC TYPE
    WASH WATER SOURCE
                                                COOLED CONDENSATE
    WASH FREQUENCY
                                                INTERMITTENT
    WASH RATE - L/S
                                                    3.2
                                                               ( 50 GAL/MIN)
** REHEATER
                                                 3
    NUMBER
    GENERIC TYPE
                                                DIRECT COMBUSTION
    SPECIFIC TYPE
                                                EXTERNAL COMBUSTION CHAMBER
    TRADE NAME/COMMON TYPE
                                                NATURAL GAS
    TEMPERATURE INCREASE - C
                                                  27.8
                                                               ( 50 F)
    INLET FLUE GAS FLOW RATE - CU. M/S
                                                              ( 230000 ACFM)
                                                  108.54
    INLET FLUE GAS TEMPERATURE - C
                                                  54.4
                                                              ( 130 F)
    OUTLET FLUE GAS TEMPERATURE - C
                                                               ( 185 F)
                                                   85.0
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                ND
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                NR
 ** FANS
    NUMBER
    NUMBER OF SPARES
                                                 Λ
    DESIGN
                                                CENTRIFUGAL
    SUPPLIER
                                                ROBINSON
    FUNCTION
                                                BOOSTER
    APPLICATION
                                                INDUCED DRAFT
    SERVICE
                                                DRY
    FLUE GAS FLOW RATE - CU.M/S
                                                 139.21
                                                               ( 295000 ACFM)
    FLUE GAS TEMPERATURE - C
                                                  215.6
                                                               ( 420 F)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                CARBON STEEL
 ** DAMPERS
    FUNCTION
                                                NR
    GENERIC TYPE
                                                NR
    SPECIFIC TYPE
                                                NR
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                NR
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                NR
    LINER GENERIC MATERIAL TYPE
                                                NR
    LINER SPECIFIC MATERIAL TYPE
                                                NR
 ** DUCTWORK
    DIMENSIONS
                                                8.0 X 8.0
     SHELL GENERIC MATERIAL TYPE
                                                CARBON STEEL
     SHELL SPECIFIC MATERIAL TYPE
                                                AISI 1110
     LINER GENERIC MATERIAL TYPE
                                                ORGANIC
                                                FIBER-REINFORCED POLYESTER
     LINER SPECIFIC MATERIAL TYPE
 ** REAGENT PREPARATION EQUIPMENT
    FUNCTION
                                                MIX TANK
    DEVICE
                                                N/A
    DEVICE TYPE
                                                AGITATED TANK
 ** TANKS
    SERVICE
                                                NUMBER
    ΝR
                                                ****
 ** PUMPS
    SERVICE
                                                NUMBER
    ABSORBER RECIRCULATION
                                                ****
** SOLIDS CONCENTRATING/DEWATERING
    DEVICE
                                                NONE
*** SALEABLE BYPRODUCTS
    NATURE
                                                SULFURIC ACID
    FULL LOAD QUANTITY - M T/H
                                                   11.34
                                                               ( 12.50 TPH)
```

DELMARVA POWER & LIGHT: DELAWARE CITY 3 (CONT.)

QUALITY - % 93.0
DISPOSITION MARKETED

*** SLUDGE

** TREATMENT

METHOD N/A
DEVICE N/A
PROPRIETARY PROCESS N/A

** DISPOSAL

NATURE FINAL TYPE POND

SITE TREATMENT CLAY LINING

** PROCESS CONTROL AND INSTRUMENTATION

CHEMICAL PARAMETERS PH, SOLIDS, SP.G., CONC.
MONITOR LOCATION GAS OUTLET, SOLUTION OUTLET
PROCESS CONTROL MANNER AUTOMATIC
PROCESS CHEMISTRY MODE FEEDBACK

** WATER BALANCE

WATER LOOP TYPE CLOSED

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

5/80 SYSTEM 100.0 100.0 100.0 32.3 744 240 240

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM BEGAN INITIAL AND COMMERCIAL OPERATIONS ON MAY 22, 1980. NO MAJOR PROBLEMS WERE ENCOUNTERED DURING STARTUP OR THROUGH THE REST OF THE MONTH.

6/80 SYSTEM 86.4 86.4 86.4 86.4 720 720 622

** PROBLEMS/SOLUTIONS/COMMENTS

REPAIRS WERE MADE TO A LEAK AND DAMAGED CHEVRON PACKING IN THE MIST ELIM-INATOR DURING JUNE.

7/80 SYSTEM 95.3 95.3 95.3 95.3 744 744 709

** PROBLEMS/SOLUTIONS/COMMENTS

SOME FGD SYSTEM OUTAGE TIME DURING THE MONTH WAS CAUSED BY LEAKS IN THE MIST ELIMINATOR THAT NEEDED REPAIR.

AN ELECTRICAL FAILURE IN THE SHUTDOWN INSTRUMENTATION CAUSED THE FGD SYSTEM TO BE OUT OF SERVICE PART OF THE MONTH.

8/80 SYSTEM 73.3 73.3 73.3 73.3 744 744 545

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS OUT OF SERVICE FOR PART OF THE MONTH TO REPAIR THE PRESCRUBBER MIST ELIMINATOR.

9/80 SYSTEM 46.4 46.4 46.4 720 720 334

744

744

329

DELMARVA POWER & LIGHT: DELAWARE CITY 3 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

#### ** PROBLEMS/SOLUTIONS/COMMENTS

FGD SYSTEM OUTAGE TIME OCCURRED DUE TO THE NECESSARY REPAIR OF THE INLET EXPANSION JOINTS DURING SEPTEMBER.

PROBLEMS WERE ENCOUNTERED WITH THE PRE-MIST ELIMINATOR CAUSING ADDITIONAL OUTAGE TIME.

44.2

ADDITIONAL OUTAGE TIME WAS NECESSARY TO MAKE REPAIRS TO THE BOOSTER BLOWER ROTOR.

44.2

44.2

** PROBLEMS/SOLUTIONS/COMMENTS

10/80 SYSTEM

DURING OCTOBER SOME OF THE OUTAGE TIME WAS DUE TO REPAIRS OF THE BOOSTER BLOWER ROTOR.

REPAIR WORK ON THE DUCT EXPANSION JOINTS ALSO CAUSED SOME OUTAGE TIME DURING THE MONTH.

DURING OCTOBER PROBLEMS WERE ENCOUNTERED WITH THE MIST ELIMINATORS.

11/80 SYSTEM .0 .0 .0 .0 720 279

44.2

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER WAS OUT OF SERVICE FOR APPROXIMATELY 465 HOURS FOR AN ANNUAL SCHEDULED MAINTENANCE OVERHAUL DURING NOVEMBER. START-UP OF THE FGD SYSTEM WAS DELAYED DUE TO THE LATE DELIVERY OF PIECES OF THE MIST ELIMINATOR INTERNALS.

12/80 SYSTEM 82.4 79.2 79.2 79.2 744 744 589

** PROBLEMS/SOLUTIONS/COMMENTS

APPROXIMATELY 107 HOURS OF OUTAGE TIME IN DECEMBER WERE DUE TO LEAKS IN THE PRESATURATOR CIRCULATING PIPING.

1/81 SYSTEM 64.0 64.0 64.0 744 744 479

** PROBLEMS/SOLUTIONS/COMMENTS

DURING JANUARY PROBLEMS WERE ENCOUNTERED WITH LEAKS IN THE RECIRCULATION PIPES AND THE MIST ELIMINATOR CAUSING OUTAGE TIME.

2/81 SYSTEM 88.0 88.0 88.0 88.0 672 672 590

** PROBLEMS/SOLUTIONS/COMMENTS

FAILURE OF THE RECIRCULATION PUMPS CAUSED SOME OUTAGE TIME DURING FEBRUARY.

LEAKS IN THE RECIRCULATION PIPES CAUSED ADDITIONAL OUTAGE TIME DURING THE MONTH.

3/81 SYSTEM 83.3 83.3 83.3 744 744 620

** PROBLEMS/SOLUTIONS/COMMENTS

DURING MARCH DOWNTIME WAS EXPERIENCED DUE TO CONTINUING REPAIRS TO THE RECTRON ATTON PIPES.

ADDITIONAL OUTAGE TIME WAS DUE TO THE REPAIRS TO THE MIST ELIMINATOR.

DELMARVA POWER & LIGHT: DELAWARE CITY 3 (CONT.)

._____PERFORMANCE DATA-----PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS FACTOR 720 720 669 93.0 93.0 93.0 4/81 SYSTEM 93.0 ** PROBLEMS/SOLUTIONS/COMMENTS DURING APRIL SOME OUTAGE TIME WAS DUE TO REPAIRS ON A HOLE IN THE ESP CELL. ADDITIONAL OUTAGE TIME WAS DUE TO THE REPLACEMENT OF A PRESATURATOR SPRAY NOZZLE. 744 5/81 SYSTEM 76.1 76.1 76.1 76.1 744 566 ** PROBLEMS/SOLUTIONS/COMMENTS DURING MAY THE PRESATURATOR SHELL MATERIAL FAILED AND AN OUTAGE WAS NECES-SARY TO REPAIR THE HOLE. THE PRESATURATOR SPRAY NOZZLE FAILED ACCOUNTING FOR ADDITIONAL OUTAGE TIME. 100.0 100.0 720 720 720 6/81 SYSTEM 100.0 100.0 ** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO PROBLEMS WERE ENCOUNTERED DURING JUNE. 7/81 SYSTEM 98.9 98.9 98.9 98.9 744 744 736 8/81 SYSTEM 100.0 100.0 100.0 100.0 744 744 744 89 9 9/81 SYSTEM 90.0 90.0 89.9 720 719 647 ** PROBLEMS/SOLUTIONS/COMMENTS THE FGD SYSTEM WAS OFF LINE FOR PART OF SEPTEMBER TO REPAIR THE ABSORBER MIST ELIMINATOR. 10/81 SYSTEM 78.2 86.3 86.4 78.2 744 674 582 ** PROBLEMS/SOLUTIONS/COMMENTS DURING OCTOBER SOME OUTAGE TIME WAS REQUIRED FOR MIST ELIMINATOR REPAIR. THE MIST ELIMINATOR WAS DAMAGED BY HEAT FROM THE REHEATER DURING AN ELECTRICAL SHUTDOWN IN SEPTEMBER. CARRYOVER INTO THE OVERHEAD DUCT CAUSED A SYSTEM SHUTDOWN FOR CLEANING. THE UNIT WAS SHUTDOWN ON OCTOBER 27 FOR AN OVERHAUL. 11/81 SYSTEM 42.2 88.9 88.9 42.2 720 342 304 ** PROBLEMS/SOLUTIONS/COMMENTS THE UNIT OVERHAUL CONTINUED INTO NOVEMBER. FOLLOWING STARTUP IT WAS NECESSARY TO TAKE THO SHORT SHUTDOWNS TO UNPLUG A WATER LINE. 12/81 SYSTEM 95.3 95.3 95.3 95.3 744 744 709 ** PROBLEMS/SOLUTIONS/COMMENTS

84.8

OR THE FGD SYSTEM.

84.8

84.8

1/82 SYSTEM

DURING DECEMBER NO MAJOR PROBLEMS WERE ENCOUNTERED WITH EITHER THE BOILER

744

744

631

84.8

DELMARVA POWER & LIGHT: DELAWARE CITY 3 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

302 PART. HOURS HOURS HOURS HOURS HOURS HOURS

** PROBLEMS/SOLUTIONS/COMMENTS

DURING JANUARY SOME OUTAGE TIME WAS DUE TO A STEAM SHORTAGE.

THE ESP DRAIN LINES WERE CLEANED DURING THE MONTH.

2/82 SYSTEM 97.2 97.2 97.2 97.2 672 672 653

** PROBLEMS/SOLUTIONS/COMMENTS

DURING FEBRUARY THE PURGE LINE WAS REPAIRED.

3/82 SYSTEM 56.8 56.8 56.8 56.8 744 744 423

** PROBLEMS/SOLUTIONS/COMMENTS

DURING MARCH PROBLEMS WITH THE SOLUTION REGENERATION SECTION HINDERED THE FGD SYSTEM OPERATION PART OF THE TIME.

4/82 SYSTEM 78.9 78.9 78.9 78.9 720 720 568

** PROBLEMS/SOLUTIONS/COMMENTS

DURING APRIL THE SYSTEM WAS SHUT DOWN FOR 152 HOURS TO BALANCE THE BOOSTER BLOWER.

5/82 SYSTEM 96.4 96.4 96.4 744 717

** PROBLEMS/SOLUTIONS/COMMENTS

DURING MAY THE FGD SYSTEM OPERATED WITH NO MAJOR PROBLEMS BEING ENCOUNTER-

<del>--</del> ·

6/82 SYSTEM 99.4 99.4 99.4 99.4 720 720 716

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE EXPERIENCED DURING JUNE.

7/82 SYSTEM 90.7 90.7 90.7 90.7 744 744 675

** PROBLEMS/SOLUTIONS/COMMENTS

A LACK OF SOLUTION DUE TO EVAPORATOR PROBLEMS ACCOUNTED FOR OUTAGE TIME DURING JULY.

8/82 SYSTEM 100.0 100.0 100.0 100.0 744 744 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING AUGUST.

9/82 SYSTEM 65.7 65.7 65.7 720 720 473

** PROBLEMS/SOLUTIONS/COMMENTS

PROBLEMS WITH BOOSTER FAN VIBRATIONS RESULTED IN OUTAGE TIME DURING SEPTEMBER.

A PLUGGAGE PROBLEM IN THE ESP SEAL POTS ALSO CONTRIBUTED TO OUTAGE TIME DURING THE MONTH.

DELMARVA POWER & LIGHT: DELAWARE CITY 3 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

ADDITIONAL OUTAGE TIME WAS ATTRIBUTED TO LEAKS IN THE PRESATURATOR

CIRCULATION PIPING.

10/82 SYSTEM 44.6 92.0 92.0 44.6 744 361 332

** PROBLEMS/SOLUTIONS/COMMENTS

DURING OCTOBER THE UNIT WAS DOWN FOR AN ANNUAL INSPECTION.

11/82 SYSTEM 78.9 97.9 97.9 78.9 720 580 568

** PROBLEMS/SOLUTIONS/COMMENTS

DURING NOVEMBER THE UNIT WAS DOWN FOR AN ANNUAL INSPECTION.

12/82 SYSTEM 98.7 98.7 98.7 98.7 744 744 734

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED

DURING DECEMBER.

1/83 SYSTEM 93.4 93.0 93.0 88.0 744 704 655

** PROBLEMS/SOLUTIONS/COMMENTS

AN OUTAGE OCCURRED DURING THE MONTH DUE TO THE CLEANING OF THE PRESATURATOR

SUCTION SCREENS.

THE REPAIR OF A CRACKED NOZZLE ON THE PRESATURATOR CAUSED ADDITIONAL DOWN

TIME DURING JANUARY.

2/83 SYSTEM 100.0 100.0 100.0 100.0 672 672 672

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED

DURING FEBRUARY.

3/83 SYSTEM 94.8 94.8 94.8 744 745 705

** PROBLEMS/SOLUTIONS/COMMENTS

AN OUTAGE OCCURRED DURING MARCH DUE TO THE CLEANING OF A PRESATURATOR

CIRCULATION PUMP SUCTION SCREEN.

THE REPAIR OF BROKEN WIRE IN AN ESP ALSO RESULTED IN DOWN TIME DURING

MARCH.

4/83 SYSTEM 99.3 99.3 99.3 720 720 715

5/83 SYSTEM 99.3 99.3 99.3 744 744 739

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED

DURING APRIL AND MAY.

6/83 SYSTEM 100.0 100.0 100.0 100.0 720 720

DELMARVA POWER & LIGHT: DELAWARE CITY 3 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED

DURING JUNE.

7/83 SYSTEM 92.5 92.5 92.5 92.5 744 744 688

** PROBLEMS/SOLUTIONS/COMMENTS

UNIT 3 WAS DOWN DURING PART OF JULY FOR ESP REPAIRS.

THE UNIT WAS DOWN DURING THE MONTH FOR REMOVAL OF SOLIDS BUILD UP IN THE

PRESCRUBBER.

8/83 SYSTEM 93.0 93.0 100.0 93.0 744 744 692

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED

DURING AUGUST.

9/83 SYSTEM 86.3 86.3 86.3 720 720 621

** PROBLEMS/SOLUTIONS/COMMENTS

UNIT 3 WAS DOWN DURING PART OF SEPTEMBER TO REPAIR LEAKS ON THE PRESCRUBBER SPRAY NOZZLE FLANGE. IN ADDITION, A CERAMIC SPRAY NOZZLE TIP FAILED

TWICE DURING THIS PERIOD.

10/83 SYSTEM 100.0 97.4 97.4 84.1 744 643 626

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURING OCTOBER.

11/83 SYSTEM 58.6 89.4 89.4 53.8 720 433 387

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT AN ANNUAL BOILER OUTAGE TOOK PLACE DURING NOVEM-

BER.

12/83 SYSTEM 58.7 78.7 78.7 58.7 744 555 437

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS DOWN DURING PART OF DECEMBER FOR AN ANNUAL OUTAGE.

FGD SYSTEM OUTAGE TIME DURING DECEMBER WAS DUE IN PART TO A LACK OF SODIUM

SULFITE ABSORBING SOLUTION RESULTING FROM EVAPORATOR PROBLEMS.

1/84 SYSTEM 95.6 95.6 95.6 95.6 744 744 711

** PROBLEMS/SOLUTIONS/COMMENTS

A LACK OF ABSORBING SOLUTION DUE TO EVAPORATOR CIRCULATING PUMP PROBLEMS AND PLUGGED EVAPORATOR SOLUTION HEADERS LIMITED THE BURNING OF HIGH SULFUR

COKE DURING JANUARY.

2/84 SYSTEM 97.6 97.6 97.6 97.6 696 696 679

DELMARVA POWER & LIGHT: DELAWARE CITY 3 (CONT.)

_____PERFORMANCE DATA------PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE REPORTED DURING FEBRUARY.

744 744 84.5 84.5 84 5 3/84 SYSTEM 84.5

** PROBLEMS/SOLUTIONS/COMMENTS

PRESATURATOR CLEANING ACCOUNTED FOR OUTAGE TIME DURING THE MONTH.

PRESATURATOR CIRCULATION PUMP REPAIRS WERE MADE DURING MARCH.

FGD SYSTEM OUTAGE TIME DURING MARCH WAS DUE IN PART TO THE REPAIR OF A BROKEN INSULATOR ON THE ESP.

720 87.1 74.0 667 533 4/84 SYSTEM 89.0 79.9

** PROBLEMS/SOLUTIONS/COMMENTS

LEAKS IN THE MIST ELIMINATOR SHELL WERE REPAIRED DURING APRIL.

LEAKS IN THE BOOSTER FAN DISCHARGE DUCTWORK WERE REPAIRED DURING APRIL.

THE FGD SYSTEM WAS DOWN DURING PART OF THE MONTH TO CLEAN THE PRESATURATOR.

A BOILER TUBE LEAK ACCOUNTED FOR 108 HOURS OF DOWN TIME DURING APRIL.

86.8 744 744 646 5/84 SYSTEM 86.8 86.8 86.8

** PROBLEMS/SOLUTIONS/COMMENTS

THE FAILURE OF A PRESATURATOR CIRCULATING PUMP MOTOR OCCURRED DURING MAY.

FAILURE OF A RUBBER LINED PIPE IN THE PRESATURATOR CIRCUIT RESULTED IN DOWN TIME DURING MARCH.

PRESATURATOR PLUGGING PROBLEMS WERE REPORTED DURING MAY.

6/84 SYSTEM 720

7/84 SYSTEM 744

8/84 SYSTEM 744

9/84 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE PERIOD OF JUNE THROUGH SEPTEMBER 1984.

# SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

DESERET GEN & TRANS COMPANY NAME PLANT NAME BONANZA UNIT NUMBER VERNAL CITY UTAH STATE REGULATORY CLASSIFICATION ***** PARTICULATE EMISSION LIMITATION - NG/J (***** LB/MMBTU) SO2 EMISSION LIMITATION - NG/J (***** LB/MMBTU) (***** LB/MMBTU) ***** NOX EMISSION LIMITATION - NG/J 800 NET PLANT GENERATING CAPACITY - MW 410 388 400 GROSS UNIT GENERATING CAPACITY - MW NET UNIT GENERATING CAPACITY W/FGD - MW NET UNIT GENERATING CAPACITY WO/FGD - MW EQUIVALENT SCRUBBED CAPACITY - MW 410 ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER ***** BOILER TYPE PULVERIZED COAL BOILER SERVICE LOAD BASE BOILER SERVICE LUAU
DESIGN BOILER FLUE GAS FLOW - CU.M/S ****** (***** ACFM) BOILER FLUE GAS TEMPERATURE - C ***** (**** F) ***** STACK HEIGHT - M (**** FT) STACK SHELL NR ***** STACK TOP DIAMETER - M (**** FT) ** FUEL DATA FUEL TYPE COAL FUEL GRADE BITUMINOUS AVERAGE HEAT CONTENT - J/G 24423. ( 10500 BTU/LB) RANGE HEAT CONTENT - BTU/LB ***** AVERAGE ASH CONTENT - % 10.00 RANGE ASH CONTENT - % ***** 8.50 AVERAGE MOISTURE CONTENT - % RANGE MOISTURE CONTENT - % ***** AVERAGE SULFUR CONTENT - % .50 ***** RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % ****** RANGE CHLORIDE CONTENT - % ***** *** PARTICLE CONTROL ** FABRIC FILTER NUMBER SUPPLIER **ECOLAIRE** ** PARTICLE SCRUBBER NUMBER GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL N/A N/A LINER GENERIC MATERIAL LINER SPECIFIC MATERIAL N/A GAS CONTACTING DEVICE TYPE N/A *** FGD SYSTEM ** GENERAL DATA THROWAWAY PRODUCT SALEABLE PRODUCT/THROWAWAY PRODUCT WET SCRUBBING SO2 REMOVAL MODE PROCESS TYPE LIMESTONE SYSTEM SUPPLIER COMBUSTION ENGINEERING BURNS & MCDONNELL A-F FTPM DEVELOPMENT LEVEL FULL SCALE NEW NEW/RETROFIT UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.60 UNIT DESIGN SO2 REMOVAL EFFICIENCY - X 95.00

2.9

ENERGY CONSUMPTION %

## DESERET GEN & TRANS: BONANZA 1 (CONT.)

	CUMPENT CTATUS	1
	CURRENT STATUS	12/84
	COMMERCIAL START-UP	
	INITIAL START-UP .	9/84
	CONTRACT AWARDED	7/80
**	DESIGN AND OPERATING PARAMETERS	
××	QUENCHER/PRESATURATOR	
~~	CONSTRUCTION MATERIAL GENERIC TYPE	NR
		NR
	CONSTRUCTION MATERIAL SPECIFIC TYPE	NR
**	ABSORBER	
	GENERIC TYPE	NR
	SPECIFIC TYPE	NR
	TRADE NAME/COMMON TYPE	NR
	SHELL GENERIC MATERIAL	NR
	SHELL SPECIFIC MATERIAL	NR
	SHELL MATERIAL TRADE NAME/COMMON TYPE	NR 
	LINER GENERIC MATERIAL	NR
	LINER SPECIFIC MATERIAL	NR
	LINER MATERIAL TRADE NAME/COMMON TYPE	NR
××	MIST ELIMINATOR	
	PRE-MIST ELIMINATOR/MIST ELIMINATOR	NR
	GENERIC TYPE	NB.
		NR
	SPECIFIC TYPE	
	TRADE NAME/COMMON TYPE	NR
	CONSTRUCTION MATERIAL GENERIC TYPE	NR
	CONSTRUCTION MATERIAL SPECIFIC TYPE	NR
××	REHEATER	
	GENERIC TYPE	NR
	SPECIFIC TYPE	NR
	TRADE NAME/COMMON TYPE	NR
	CONSTRUCTION MATERIAL GENERIC TYPE	NR
	CONSTRUCTION MATERIAL SPECIFIC TYPE	NR
	<b>*</b> * * * * * * * * * * * * * * * * * *	
**	FANS	
	DESIGN	NR
	FUNCTION	NA
	APPLICATION	NR
	SERVICE	NA
	CONSTRUCTION MATERIAL GENERIC TYPE	NA
××	DAMPERS	
	FUNCTION	NR
	GENERIC TYPE	
		NR 
	SPECIFIC TYPE	NR
	CONSTRUCTION MATERIAL GENERIC TYPE	NR
	CONSTRUCTION MATERIAL SPECIFIC TYPE	NR
	LINER GENERIC MATERIAL TYPE	NR
	LINER SPECIFIC MATERIAL TYPE	
	CINCK SPECIFIC MATERIAL TIPE	NR
	LINER SPECIFIC MATERIAL TYPE	NR
××	DUCTWORK	NR
××	DUCTWORK	
××	DUCTWORK SHELL GENERIC MATERIAL TYPE	MR
**	DUCTWORK SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE	NR NR
××	DUCTWORK SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE	NR NR NR
**	DUCTWORK SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE	NR NR
	DUCTWORK SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	NR NR NR
	DUCTWORK SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE REAGENT PREPARATION EQUIPMENT	NR NR NR NR
	DUCTWORK SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE REAGENT PREPARATION EQUIPMENT FUNCTION	NR NR NR
	DUCTWORK SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE	NR NR NR NR
	DUCTWORK SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE REAGENT PREPARATION EQUIPMENT FUNCTION	NR NR NR NR
**	DUCTWORK SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE  REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE DEVICE TYPE	NR NR NR NR NR COMPARTMENTED
**	DUCTWORK SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE	NR NR NR NR NR COMPARTMENTED
**	DUCTWORK SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE  REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE DEVICE TYPE	NR NR NR NR NR COMPARTMENTED NA
**	DUCTWORK SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE  REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE DEVICE TYPE  TANKS	NR NR NR NR NR COMPARTMENTED
**	DUCTWORK SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE  REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE DEVICE TYPE  TANKS SERVICE	NR NR NR NR NR COMPARTMENTED NA

### DESERET GEN & TRANS: BONANZA 1 (CONT.)

** PUMPS

SERVICE NUMBER

** SOLIDS CONCENTRATING/DEWATERING

DEVICE THICKENER NUMBER 1

** SOLIDS CONCENTRATING/DEWATERING

DEVICE VACUUM FILTER

NUMBER

*** SLUDGE

** TREATMENT

METHOD DEWATERED
DEVICE NR
PROPRIETARY PROCESS N/A

** DISPOSAL

NATURE FINAL
TYPE LANDFILL
LOCATION ON-SITE
SITE TREATMENT NONE

** WATER BALANCE

WATER LOOP TYPE CLOSED

SOURCE OF MAKEUP WATER COOLING TOWER BLOWDOWN

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

9/84 SYSTEM 720

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT INITIAL START-UP OF THE FGD SYSTEM COMMENCED IN SEPTEMBER 1984.

# SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

DUQUESNE LIGHT COMPANY NAME FIRAMA PLANT NAME 1-4 UNIT NUMBER ELRAMA CITY PENNSYLVANIA STATE 258. ( .080 LB/MMBTU)
258. ( .600 LB/MMBTU)

****** (****** LB/MMBTU)

487
510 REGULATORY CLASSIFICATION PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW
NET UNIT GENERATING CAPACITY W/FGD - MW
NET UNIT GENERATING CAPACITY WO/FGD - MW 487 494 510 EQUIVALENT SCRUBBED CAPACITY - MW ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER BABCOCK & WILCOX BOILER TYPE PULVERTZED COAL BOILER SERVICE LOAD BASE DESIGN BOILER FLUE GAS FLOW - CU.M/S
BOILER FLUE GAS TEMPERATURE - C 972.11 (2060000 ACFM) 148.9 (300 F) 121. (398 FT) STACK HEIGHT - M CONCRETE 7.9 ( 26.0 FT) STACK SHELL STACK TOP DIAMETER - M ** FUEL DATA FUEL TYPE COAL COAL BITUMINOUS 24907. ( 11568 BTU/LB) 21500-12500 FUEL GRADE AVERAGE HEAT CONTENT - J/G RANGE HEAT CONTENT - BTU/LB 16.80 AVERAGE ASH CONTENT - % RANGE ASH CONTENT % 14.0-18.3 AVERAGE MOISTURE CONTENT - % 5.93 RANGE MOISTURE CONTENT % 4.30-7.06 AVERAGE SULFUR CONTENT - % 2.05 RANGE SULFUR CONTENT - %
AVERAGE CHLORIDE CONTENT - % 1.49-2.91 .04 RANGE CHLORIDE CONTENT - % 0.03-0.05 *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER 4 NUMBER OF SPARES Ω TYPE MULTICLONE SUPPLIER RESEARCH-COTTRELL [1, 2, & 31; JOY WESTERN [4] INLET FLUE GAS CAPACITY CU.M/S 972.1 (2060000 ACFM)
INLET FLUE GAS TEMPERATURE - C 148.9 (300 F)
PRESSURE DROP - KPA .7 (3. IN-H2O)
PARTICLE REMOVAL EFFICENCY -% 95.0 ** ESP NUMBER 10 NUMBER OF SPARES 0 COLD SIDE SUPPLIER

SUPPLIER

RESEARCH COTTRELL [1, 2, & 31; JOY WESTERN [4]

INLET FLUE GAS CAPACITY - CU.M/S

INLET FLUE GAS TEMPERATURE - C

148.9 ( 300 F)

PRESSURE DROP - KPA

2 ( 1. IN-H20) .2 95.0 PARTICLE REMOVAL EFFICENCY - % ** PARTICLE SCRUBBER GENERIC TYPE N/A SPECIFIC TYPE N/A *** FGD SYSTEM

#### DUQUESNE LIGHT: ELRAMA 1-4 (CONT.)

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** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                               THROWAWAY PRODUCT
   SO2 REMOVAL MODE
                                               WET SCRUBBING
   PROCESS TYPE
                                               LIME
   PROCESS ADDITIVES
                                               MAGNESIUM OXIDE, SODIUM
   SYSTEM SUPPLIER
                                               GE ENVIRONMENTAL SERVICES
   A-F FIRM
                                               GIBBS & HILL
   DEVELOPMENT LEVEL
                                               FULL SCALE
   NEW/RETROEIT
                                               RETROETT
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.30
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                  83.00
   ENERGY CONSUMPTION - %
                                                  1.4
   CURRENT STATUS
                                                1
   COMMERCIAL START-UP
                                               10/75
   INITIAL START-UP
                                               10/75
   CONTRACT AWARDED
                                               12/70
** DESIGN AND OPERATING PARAMETERS
   DESIGN COAL SULFER CONTENT - %
                                                   2.20
   DESIGN COAL HEAT CONTENT - J/G
                                               26749.0
                                                              ( 11500 BTU/LB)
   DESIGN COAL ASH CONTENT - %
                                                  17.00
   DESIGN MOISTURE CONTENT - % DESIGN CHLORIDE CONTENT %
                                                   6.00
                                                    .03
   OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                296.0
** QUENCHER/PRESATURATOR
   NUMBER
                                                0
** ABSORBER
   NUMBER
                                                5
   NUMBER OF SPARES
                                                1
                                               VENTURI TOWER
   GENERIC TYPE
    SPECIFIC TYPE
                                               VARIABLE-THROAT/TOP-ENTRY PLUMB BOB
    TRADE NAME/COMMON TYPE
                                               N/A
   SUPPLIER
                                               GE ENVIRONMENTAL SERVICES
   DIMENSIONS - FT
                                               31.3 X 66.4
   SHELL GENERIC MATERIAL
                                               CARBON STEEL; STAINLESS STEEL [ABSORBER INTERNAL
   SHELL SPECIFIC MATERIAL
                                               AISI 1110; AUSTENITIC
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                               N/A; TYPE 316L
   LINER GENERIC MATERIAL
                                               ORGANIC; INORGANIC
                                               MAT-REINFORCED POLYESTER; GLASS FLAKE-FILLED POL
   LINER SPECIFIC MATERIAL
   LINER MATERIAL TRADE NAME/COMMON TYPE
                                               CEILCRETE 2500AR; FLAKELINE 103; ACID RESISTANT
   GAS CONTACTING DEVICE TYPE
                                               NONE
   NUMBER OF CONTACTING ZONES
                                                1
   LIQUID RECIRCULATION RATE - LITER/S
                                                1071.
                                                              (17000 GPM)
   L/G RATIO - L/CU.M
                                                   4.4
                                                              ( 33.0 GAL/1000 ACF)
   GAS-SIDE PRESSURE DROP KPA
                                                   2.0
                                                              ( 8.0 IN-H20)
   SUPERFICAL GAS VELOCITY - M/SEC
                                                  45.7
                                                              (150.0 FT/S)
   INLET GAS FLOW CU. M/S
                                                 243.03
                                                              ( 515000 ACFM)
   INLET GAS TEMPERATURE - C
                                                 148.9
                                                              ( 300 F)
   SO2 REMOVAL EFFICIENCY - X
                                                  83.0
   PARTICLE REMOVAL EFFICENCY - %
                                                  94.0
** MIST ELIMINATOR
                                               PRIMARY COLLECTOR [EXTERNAL]
   PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                                5
   NUMBER PER SYSTEM
   NUMBER OF SPARES PER SYSTEM
                                                1
   NUMBER PER MODULE
                                               IMPINGEMENT
   GENERIC TYPE
   SPECIFIC TYPE
                                               BAFFLE
   TRADE NAME/COMMON TYPE
                                               OPEN VANE [SLAT]
   MANUFACTURER
                                               HEIL
                                               HORIZONTAL
   CONFIGURATION
   NUMBER OF STAGES
                                                   1
   NUMBER OF PASSES PER STAGE
                                                   4
   DISTANCE BETWEEN VANES - CM
                                                   7.6
                                                              ( 3.00 IN)
   VANE ANGLES DEGREES
                                                 90
   PRESSURE DROP - KPA
                                                    . 0
                                                              ( .2 IN-H20)
   SUPERFICAL GAS VELOCITY - M/S
                                                              ( 11.0 FT/S)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              ORGANIC
```

FIBER-REINFORCED POLYESTER

CONSTRUCTION MATERIAL SPECIFIC TYPE

```
DUQUESNE LIGHT: ELRAMA 1-4 (CONT.)
```

FRESH MAKEUP WATER OR THICKENER OVERFLOW WASH WATER SOURCE TOP-MANUAL ONCE/WEEK WASH FREQUENCY ** REHEATER DIRECT COMBUSTION GENERIC TYPE IN-LINE BURNER SPECIFIC TYPE TRADE NAME/COMMON TYPE JIO 30 F) 16.7 TEMPERATURE INCREASE - C CONSTRUCTION MATERIAL GENERIC TYPE NR NR CONSTRUCTION MATERIAL SPECIFIC TYPE ** FANS 5 NUMBER 1 NUMBER OF SPARES CENTRIFUGAL DESIGN GREEN FUEL ECONOMIZER SUPPLIER BOOSTER **FUNCTION** INDUCED DRAFT APPLICATION SERVICE WFT 259.54 ( 550000 ACFM) FLUE GAS FLOW RATE - CU.M/S FLUE GAS TEMPERATURE - C 54.4 ( 130 F) PRESSURE DRCP - KPA 7.0 (23.0 IN-H20) CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL; HIGH ALLOY; HIGH ALLOY; STAINLESS ** DAMPERS NUMBER SHUT-OFF **FUNCTION** GENERIC TYPE BUTTERFLY SPECIFIC TYPE NR MANUFACTURER NP MODULATION OPEN/CLOSED SEAL AIR FLOW - CU. M/S .00 0 ACFM) ( SERVICE CONDITIONS 300 CONSTRUCTION MATERIAL GENERIC TYPE STAINLESS STEEL/CARBON STEEL CONSTRUCTION MATERIAL SPECIFIC TYPE AUSTENITIC; AISI 1110 LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DAMPERS NUMBER 5 FUNCTION SHUT-OFF GENERIC TYPE LOUVER SPECIFIC TYPE PARALLEL BLADE MULTILOUVER MANUFACTURER ALLIS-CHALMERS MODULATION OPEN/CLOSED SEAL AIR FLOW - CU. M/S .00 ( 0 ACFM) SERVICE CONDITIONS ND CONSTRUCTION MATERIAL GENERIC TYPE STAINLESS STEEL/CARBON STEEL CONSTRUCTION MATERIAL SPECIFIC TYPE AUSTENITIC; AISI 1110 LINER GENERIC MATERIAL TYPE ORGANIC LINER SPECIFIC MATERIAL TYPE GLASS FLAKE-FILLED POLYESTER ** DAMPERS NUMBER 5 FUNCTION SHUT-OFF GENERIC TYPE LOUVER SPECIFIC TYPE PARALLEL BLADE MULTILOUVER MANUFACTURER ALLIS-CHALMERS MODULATION OPEN/CLOSED SEAL AIR FLOW - CU. M/S .00 ( 0 ACEM SERVICE CONDITIONS NR CONSTRUCTION MATERIAL GENERIC TYPE STAINLESS STEEL/CARBON STEEL CONSTRUCTION MATERIAL SPECIFIC TYPE AUSTENITIC; AISI 1110 LINER GENERIC MATERIAL TYPE ORGANIC LINER SPECIFIC MATERIAL TYPE GLASS FLAKE-FILLED POLYESTER ** DUCTWORK LOCATION ABSORBER INLET CONFIGURATION CIRCULAR SHELL GENERIC MATERIAL TYPE CARBON STEEL

**AISI 1110** 

SHELL SPECIFIC MATERIAL TYPE

```
DUQUESNE LIGHT: ELRAMA 1-4 (CONT.)
     LINER GENERIC MATERIAL TYPE
                                                NONE
     LINER SPECIFIC MATERIAL TYPE
                                                N/A
** DUCTWORK
                                                ABSORBER OUTLET
    LOCATION
    CONFIGURATION
                                                RECTANGULAR
     SHELL GENERIC MATERIAL TYPE
                                                CARBON STEEL
     SHELL SPECIFIC MATERIAL TYPE
                                               AISI 1110
     LINER GENERIC MATERIAL TYPE
                                                ORGANIC
     LINER SPECIFIC MATERIAL TYPE
                                                GLASS FLAKE-FILLED POLYESTER
 ** DUCTWORK
                                                PRECOLLECTOR OUTLET
    LOCATION
    CONFIGURATION
                                                CIRCULAR
     SHELL GENERIC MATERIAL TYPE
                                                CARBON STEEL
     SHELL SPECIFIC MATERIAL TYPE
                                                AISI 1110
     LINER GENERIC MATERIAL TYPE
                                                ORGANIC
     LINER SPECIFIC MATERIAL TYPE
                                                GLASS FLAKE-FILLED POLYESTER
 ** REAGENT PREPARATION EQUIPMENT
    FUNCTION
                                                SLAKER
    DEVICE
                                                PASTE
    DEVICE TYPE
                                                N/A
    MANUFACTURER
                                                WALLACE & TIERNAN
    NUMBER
                                                 5
    NUMBER OF SPARES
    FULL LOAD DRY FEED CAPACITY - M.TONS/HR
                                                    3.6
                                                               (
                                                                   4 TPH)
    PRODUCT QUALITY - X SOLIDS
                                                   22.5
 ** TANKS
    SERVICE
                                                NUMBER
                                                -----
    THICKENER OVERFLOW
                                                   1
    LIME SLURRY DILUTION
    ABSORBER EFFLUENT HOLD
                                                   5
    THICKENER FOLMER MIX
                                                   1
    THICKENER DISTRIBUTION BOX
                                                   1
    WATER STORAGE
                                                   2
 ** PUMPS
                                                NUMBER
    SERVICE
    ABSORBER RECIRCULATION
                                                  10
    LIME SLURRY FEED
                                                   5
    THICKENER OVERFLOW
                                                   3
    THICKENER UNDERFLOW
                                                   3
 ** SOLIDS CONCENTRATING/DEWATERING
    DEVICE
                                                THICKENER
    NUMBER
                                                 2
                                                0
    NUMBER OF SPARES
    DIMENSIONS - FT
                                                120 DIA X 8.5 HIGH
    CAPACITY
                                                229500
    SHELL GENERIC MATERIAL TYPE
                                               CARBON STEEL [WALLS]; INORGANIC [BOTTOM]
                                               AISI 1110; HYDRAULICALLY-BONDED CONCRETE
    SHELL SPECIFIC MATERIAL TYPE
    LINER GENERIC MATERIAL TYPE
                                                ORSANIC
    LINER SPECIFIC MATERIAL TYPE
                                               BITUMINOUS BASE MODIFIED ASPHALT [FLOOR]; MICA F
    BELT GENERIC MATERIAL TYPE
                                               RUBBER-CLAD CARBON STEEL
                                                ABSORBER BLEED STREAM
    FEED STREAM SOURCE
    FEED STREAM CHARACTERISTICS
                                                5% SOLIDS
                                                35-40% SOLIDS
    OUTLET STREAM CHARACTERISTICS
    OVERFLOW STREAM CHARACTERISTICS
                                                0.1%
                                                TO VACUUM FILTER
    OUTLET STREAM DISPOSITION
                                                THICKENER OVERFLOW TANK
    OVERFLOW STREAM DISPOSITION
 ** SOLIDS CONCENTRATING/DEWATERING
    DEVICE
                                                VACUUM FILTER
```

2

60 TONS/HR

650 SQ FT & 750 SQ FT

NUMBER

NUMBER OF SPARES

DIMENSIONS - FT CAPACITY DUQUESNE LIGHT: ELRAMA 1-4 (CONT.) CARBON STEEL SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE AISI 1110 BELT GENERIC MATERIAL TYPE ORGANIC BELT SPECIFIC MATERIAL TYPE NYLON THICKENER UNDERFLOW FEED STREAM SOURCE 35-40% SOLIDS FEED STREAM CHARACTERISTICS 50% SOLIDS OUTLET STREAM CHARACTERISTICS OVERFLOW STREAM CHARACTERISTICS 0.1 TO SLUDGE TREATMENT OUTLET STREAM DISPOSITION COLLECTED IN A DISTRIBUTION BOX & THEN TRANSFERR OVERFLOW STREAM DISPOSITION *** SLUDGE 50.0 % ASH - DRY % OTHER COMPOUNDS - DRY 50.0 ** TREATMENT FIXATION METHOD DEVICE PUG MILL CONVERSION SYSTEMS [POZ-O-TEC] PROPRIETARY PROCESS INLET QUALITY - % 37.5 ** DISPOSAL NATURE FINAL TYPE LANDFILL LOCATION CFF-SITE SITE TRANSPORTATION METHOD TRUCK SITE TREATMENT NONE SITE SERVICE LIFE - YRS 10 ** PROCESS CONTROL AND INSTRUMENTATION PROCESS STREAM RECIRCULATING SLURRY CHEMICAL PARAMETERS PH PHYSICAL VARIABLES FLOW CONTROL LEVELS PH 7.7 MONITOR TYPE UNIVERSAL UNILOC MONITOR LOCATION INLET TANGENTIAL NOZZLE TO ABSORBER PROCESS CONTROL MANNER AUTOMATIC PROCESS CHEMISTRY MODE FEEDBACK ** WATER BALANCE WATER LOOP TYPE OPEN EFFLUENT WATER LOSS - LITERS/S 18.9 ( 300 GPM) RECEIVING WATER STREAM MONONGAHELA RIVER SOURCE OF MAKEUP WATER RIVER WATER ** CHEMICALS AND CONSUMPTION FUNCTION ABSORBENT NAME MAGNESIUM-MODIFIED LIME FRINCIPAL CONSTITUENT CAO, MGO SOURCE/SUPPLIER DRAVO CONSUMPTION 175-200 TPD UTILIZATION - % 90.0 POINT OF ADDITION SLAKER ** FGD SPARE CAPACITY INDICES ABSORBER % 25.0 MIST ELIMINATOR - % 25.0 FAN - X 25.0 SLAKER - % 67.0 EFFLUENT HOLD TANK - % 25.0 RECIRCULATION PUMP - % 25.0 THICKENER - % .0 VACUUM FILTER - % 100.0 ** FGD SPARE COMPONENT INDICES ABSORBER

MIST ELIMINATOR

FAN

SLAKER

1.0

1.0

1.0

.8

NUQUESNE LIGHT: ELRAMA 1-4 (CONT.)

EFFLUENT HOLD TANK 1.0 RECIRCULATION PUMP 1.0 THICKENER . 0 1.0 VACUUM ETLIER

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS HOURS FACTOR

0/75 SYSTEM

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE FIRST ELRAMA SCRUBBER WAS PLACED IN SERVICE ON OCTOBER 26, 1975. IT HAD BEEN SCHEDULED FOR AN EARLIER STARTUP DATE BUT BECAUSE OF THE SEVERITY AND NUMBER OF PROBLEMS ENCOUNTERED AT PHILLIPS, STARTUP WAS DELAYED UNTIL MANY OF THE PROBLEMS AT PHILLIPS WERE RESOLVED AND THE MODIFICATIONS COULD BE INCORPORATED AT BOTH STATIONS.

BOILER NO. 2 WAS INITIALLY CONNECTED TO THE FGD SYSTEM. THIS BOILER HAS AN EQUIVALENT CAPACITY OF APPROXIMATELY 100 MW AND THE EMISSIONS CAN BE HANDLED BY ONE SCRUBBER. HOWEVER, TO ENSURE RELIABILITY IN THE CASE OF A SCRUBBER MALFUNCTION, TWO SCRUBBERS ARE OPERATED AT PARTIAL LOAD TO PROTECT THE BOILER AND TURBINE GENERATOR AGAINST A TRIP-OFF.

THE BOILER OPERATED CONTINUOUSLY ON THE SCRUBBER SYSTEM THROUGH JANUARY 1976 WITH THE EXCEPTION OF TWO MINOR OUTAGES. ON FEBRUARY 4, 1976 A SECOND BOILER WAS COUPLED INTO THE SCRUBBER COMPLEX. PRESENTLY, TWO UNITS ARE THE MAXIMUM THAT CAN BE TIED INTO THE SCRUBBER PLANT. TO DATE, THE UTILITY HAS ENCOUNTERED THE USUAL MINOR STARTUP PROBLEMS AND SOME MAJOR PROBLEMS AS WELL. THE MAJOR PROBLEMS HAVE BEEN WITH FROZEN PIPES AND THICKENERS, THE LATTER INVOLVING HARDWARE AND DESIGN PROBLEMS ASSOCIATED WITH RECIRCULATION OF THE SLUDGE WITHIN THE THICKENERS TO ATTAIN 30 TO 40% SOLIDS CONCENTRATION.

10/75 SYSTEM 744 744

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE SCRUBBING SYSTEM BEGAN OPERATIONS WITH ONE BOILER CONNECTED TO THE SYSTEM (100 MW) DURING THE MONTH. THE SCRUBBING SYSTEM IS CURRENTLY IN THE SHAKEDOWN PHASE OF OPERATION.

11/75 SYSTEM 720 720

12/75 SYSTEM 744 744

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE SYSTEM IS STILL OPERATING WITH-ONE BOILER CONNECTED. THE UTILITY IS PLANNING TO CONNECT ONE OR TWO ADDITIONAL BOILERS TO THE SYSTEM IN LATE JANUARY.

1/76 SYSTEM 744 744

## ** PROBLEMS/SOLUTIONS/COMMENTS

FOUR OF THE FIVE SCRUBBER VESSELS HAVE BEEN IN SERVICE IN VARIOUS COMBINA-TIONS, AND THE SERVICE HOURS THROUGH JANUARY 31, 1976 ARE:

NO. 1 - 69 HOURS

NO. 2 - 1508 HOURS

NO. 3 - 976 HOURS NO. 4 - 838 HOURS

THE FIFTH VESSEL HAS NOT BEEN IN SERVICE BECAUSE IT IS BEING SERVICED FOR THE TRIAL INSTALLATION OF RUBBER LINED RECYCLE PUMPS.

2/76 SYSTEM 696 696

3/76 SYSTEM 744 744

DUQUESNE LIGHT: ELRAMA 1-4 (CONT.)

4/76 SYSTEM

_____PERFORMANCE DATA-------PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS FACTOR ______

720 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE SYSTEM OPERATED DURING MARCH AND APRIL WITH TWO BOILERS COUPLED INTO THE SCRUBBING SYSTEM. REVISIONS TO THE FIFTH SCRUBBING VESSEL HAVE BEEN COMPLETED AND OPERATIONS ARE PROCEEDING WITH TWO RUBBER-LINED RECYCLE PUMPS.

744 744 5/76 SYSTEM

720 720 6/76 SYSTEM

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE SYSTEM IS STILL OPERATING WITH TWO BOILERS COUPLED INTO THE SCRUBBING SYSTEM. THE IUCS SLUDGE FIXATION SYSTEM IS CONTINUING TO OPERATE AT THIS

THE FIFTH SCRUBBING VESSEL WAS TAKEN OUT OF SERVICE FOR REPAIRS AND MODIFICATIONS REQUIRED FOR THE RUBBER-LINED RECYCLE PUMPS.

THE UTILITY IS CURRENTLY CONDUCTING A PERFORMANCE TEST ON THE SCRUBBING SYSTEM IN THE TWO BOILER OPERATION MODE.

7/76 SYSTEM 744 744

744 8/76 SYSTEM 744

# ** PROBLEMS/SOLUTIONS/COMMENTS

THE FIFTH SCRUBBING VESSEL EMPLOYING TWO RUBBER-LINED RECYCLE PUMPS WAS OPERATIONAL FOR A SHORT PERIOD OF TIME DURING THE REPORTING MONTHS. TWO BOILERS REMAIN COUPLED INTO THE SCRUBBING SYSTEM. THE CONSTRUCTION OF AD-DITIONAL LIME STORAGE SILOS AND A THICKENER WILL BE REQUIRED FOR FULL SCALE OPERATION. THE UTILITY HAS SIGNED A LETTER OF INTENT WITH IUCS FOR A LONG TERM SLUDGE FIXATION SYSTEM. HIGH CALCIUM LIME IS STILL BEING EMPLOYED IN THE SCRUBBING SYSTEM.

9/76 SYSTEM 720 720

10/76 SYSTEM 744 744

# ** PROBLEMS/SOLUTIONS/COMMENTS

OPERATIONS AT THIS STATION DURING THE REPORT PERIOD PROCEEDED WITH TWO BOILERS COUPLED INTO THE FIVE-MODULE SCRUBBING SYSTEM. THE FIFTH SCRUB-BING VESSEL WAS OPERATIONAL DURING THE REPORT PERIOD WITH THE RUBBER-LINED RECYCLE PUMPS IN SERVICE. OPERATIONS ARE STILL PROCEEDING ON AN OPEN WATER-LOOP BASIS. PART OF THE THICKENER OVERFLOW IS STILL BEING DIVERTED TO THE ASH POND AND NOT RECYCLED BACK TO THE PROCESS. BECAUSE BOTH BEAVER VALLEY AND BRUCE MANSFIELD STATIONS ARE FULLY OPERATIONAL, THIS STATION HAS BEEN RELEGATED TO PEAK LOAD OPERATIONS. GENERAL LOAD OPERA-TIONS ARE FULL CAPACITY IN THE DAYTIME AND 50 TO 60% REDUCTION AT NIGHT.

TESTS WERE CONDUCTED DURING THE PERIOD TO DETERMINE PARTICULATE AND SO2 REMOVAL EFFICIENCIES. SOZ REMOVAL EFFICIENCY WAS 50%. PARTICULATE EMISSIONS WERE BEING REDUCED WELL BELOW 0.1 LB/MM BTU STANDARD (ACTUAL RESULTS: 0.04 LB/MM BTU). THESE RESULTS WERE BASED ON TWO BOILERS COUPLED INTO THE FIVE SCRUBBING MODULES WHILE BURNING MEDIUM-SULFUR (1.0 TO 2.8%) COAL. THE MECHANICAL COLLECTORS AND ESP'S WERE IN SERVICE DURING THE TESTS.

11/76 SYSTEM

720 720 DUQUESNE LIGHT: ELRAMA 1-4 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

12/76 SYSTEM 744 744

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE SCRUBBER REMAINED IN SERVICE THROUGHOUT THE REPORT PERIOD WITH TWO BOILERS COUPLED INTO THE SCRUBBING SYSTEM. A RECYCLE PUMP EVALUATION IS BEING CONDUCTED BY THE UTILITY AT BOTH PHILLIPS AND ELRAMA STATIONS.

OBSERVATIONS OF THE RUBBER-LINED RECYCLE PUMPS INDICATE SOME SEVERE ABRASION AND GOUGING HAVE OCCURRED AFTER 1000 HOURS OF SERVICE TIME.

 1/77
 SYSTEM
 744
 744

 2/77
 SYSTEM
 672
 672

 3/77
 SYSTEM
 744
 744

#### ** PROBLEMS/SOLUTIONS/COMMENTS

TESTING WITH THIOSORBIC LIME WAS CONDUCTED DURING THE PERIOD.

THE SCRUBBER PLANT CONTINUED OPERATIONS DURING JANUARY AND FEBRUARY WITH TWO BOILERS COUPLED INTO THE SYSTEM. INSTALLATION OF THE ADDITIONAL THICKENER LIME FEEDERS AND SILOS IS STILL IN PROGRESS. FULL COMPLIANCE OPERATION FOR THIS STATION IS SCHEDULED FOR EARLY 1978. THE FULL COMPLIANCE STRATEGY WILL CONSIST OF THE FOLLOWING: 83% SO2 REMOVAL FOR 2% SULFUR COAL UTILIZING THIOSORBIC LIME (6-12% MG), FIXATING THE SCRUBBER SLUDGE WITH THE IUCS POZ-O-TEC STABILIZATION METHOD AND HAULING THIS MATERIAL TO AN OFFSITE DISPOSAL/LANDFILL AREA. CURRENT SO2 AND PARTICULATE REMOVAL EFFICIENCIES ARE 50 AND 99+%, RESPECTIVELY. THE INTERIM IUCS UNIT NOW IN SERVICE CONSISTS OF THE OLD MOHAVE PROTOTYPE PLUS A VACUUM FILTER. THE STABILIZATION MATERIAL HAS BEEN UTILIZED IN A PARKING LOT CONSTRUCTION PROJECT. IUCS HAS BEEN AWARDED A 10-YEAR CONTRACT FOR THE CONTINUED USE OF THIS SYSTEM FOR FUTURE PLANT OPERATIONS.

4/77 SYSTEM 720 720 5/77 SYSTEM 744 744

# ** PROBLEMS/SOLUTIONS/COMMENTS

CONSTRUCTION OF TWO 120-FOOT DIAMETER THICKENERS IS CONTINUING. DUE TO THE GOUGING OF THE RUBBER-LINED RECYCLE PUMPS DURING THEIR TESTING, THEY HAVE BEEN REMOVED. THE UTILITY IS CONSIDERING TRYING ANOTHER SET OF RUBBER-LINED PUMPS. DUQUESNE LIGHT ALSO IS CONTINUING EFFORTS TO OBTAIN ALTERNATE LANDFILL AREAS FOR SLUDGE DISPOSAL.

6/77 SYSTEM 720 720 7/77 SYSTEM 744 744

# ** PROBLEMS/SOLUTIONS/COMMENTS

DUQUESNE LIGHT REPORTED THE FOLLOWING ITEMS FOR THE ELRAMA SCRUBBER PLANT DURING THE REPORT PERIOD:

- -TWO BOILERS (200 MW) WERE COUPLED INTO THE SCRUBBER PLANT.
- -THE INTERIM IUCS STABILIZATION UNIT (MOHAVE PROTOTYPE) CONTINUED TO FIXATE SCRUBBER WASTES.
- -CONSTRUCTION OF THE TWO ADDITIONAL THICKENERS CONTINUED (CONSTRUCTION IS ON SCHEDULE).
- -FULL PLANT COMPLIANCE IS PROJECTED FOR FEBRUARY 1978.
- -S02 REMOVAL EFFICIENCY IS APPROXIMATELY 50%.
- -ELRAMA IS OPERATING IN A BASE/INTERMEDIATE LOAD MODE (FULL LOAD DAYTIME/

DUQUESNE LIGHT: ELRAMA 1-4 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS FACTOR

HALF LOAD NIGHT-TIME). 1976 CAPACITY FACTOR WAS 69.5%.

744 744 8/77 SYSTEM

720 720 9/77 SYSTEM

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE TWO ADDITIONAL THICKENERS WERE COMPLETELY INSTALLED. THE IUCS SYSTEM WAS UPGRADED. CONSTRUCTION COMPLETION IS PROJECTED FOR FEBRUARY 1978. FULL PLANT COMPLIANCE IS PROJECTED FOR APRIL 1978.

744 744 10/77 SYSTEM

## ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE 101 WAS UNAVAILABLE ON OCTOBER 4 DUE TO A BLEED VALVE LEAK AND WAS TAKEN OUT OF SERVICE AT THE END OF THE MONTH FOR CLEANUP.

MODULE 201 WAS AVAILABLE FOR THE ENTIRE MONTH OF OCTOBER.

MODULE 301 AND 401 HAD OUTAGES IN OCTOBER RESULTING FROM A RUBBER LINING FAILURE ON AN ID FAN.

MODULE 501 EXPERIENCED RECYCLE PUMP OUTAGES IN LATE NOVEMBER.

NEW RUBBER LINED WORMEN RECYCLE PUMPS WERE INSTALLED. THE LIME HANDLING SYSTEM INSTALLATION WORK CONTINUED. THE LAST TWO BOILERS ARE EXPECTED TO BE TIED INTO THE FGD SYSTEM BY JANUARY 1978.

11/77	101	.0	.0			
	201	11.7	11.7			
	301	93.3	93.3			
	401	22.5	22.5			
	501	59.2	59.2			
	SYSTEM	46.7	46.7	72 <b>0</b>	720	336

## ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE 101, 201 AND 401 HAVE LOW OPERATIONAL HOURS BECAUSE ONLY TWO BOILER ARE TIED INTO THE FGD SYSTEM TO DATE.

THE SLUDGE HANDLING SYSTEM IS FUNCTIONING PROPERLY AND IS NOW IN FULL SER-VICE.

TUBE LEAKS FORCED A BOILER OUTAGE IN NOVEMBER.

12/77	SYSTEM			744	744	
1/78	101	94.1	94.1			
	201	90.5	90.5			
	301	5.1	5.1			
	401	24.3	24.3			
	501	3.5	3.5			
	SYSTEM	54.4	54.4	744	744	405

# ** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE PERIOD THE UTILITY REPORTED THAT A NEW WORMEN RECYCLE PUMP INSTALLED IN NOVEMBER EXPERIENCED JACK SHAFT BEARING PROBLEMS RESULTING IN REMOVAL OF SCRUBBER TRAIN 501 FROM SERVICE.

BOILER NO. 4 WAS CONNECTED, ADDING AN ADDITIONAL 176 MW OF FLUE GAS LOAD TO THE FGD SYSTEM.

DUQUESNE LIGHT: ELRAMA 1-4 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

THE IUCS SLUDGE DISPOSAL FACILITY IS IN SERVICE PRODUCING GOOD PRODUCT.
LOW LOAD AND A COAL STRIKE HAVE HAMPERED GOOD SCRUBBER OPERATIONS. SOME

2/78	101	70.8	30.4			
	201	96.2	41.2			
	301	.0	. 0			
	401	37.2	15.9			
	501	40.0	18.0			
	SYSTEM	61.1	26.4	672	288	177
3/78	SYSTEM	.0	.0	744	216	141
3/ / 0	2121111	. 0	. 0	/44	210	TAT

OUTAGE TIME HAS BEEN SCHEDULED FOR MARCH.

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE SYSTEM WAS SHUTDOWN ON FEBRUARY 11 AS A RESULT OF A COAL SHORTAGE. BOILERS 1, 2 AND 4 ARE NOW COMPLETELY CONNECTED TO THE FGD SYSTEM. BOILER 3 IS UNDERGOING AN EXTENSIVE OVERHAUL AND WILL BE CONNECTED TO THE SYSTEM IN LATE APRIL.

BOILER EXIT DAMPERS WERE LINED WITH 316 SS ON AREAS OF HIGH EROSION CAUSED BY FLYASH IMPINGEMENT DURING THE OUTAGE.

EXPANSION JOINTS IN THE UPSTREAM DUCTWORK WERE SHIELDED BY METAL PLATES WHICH WERE WELDED AT ONE END DURING THE FEBRUARY-MARCH PERIOD. EXPANSION JOINTS IN THE DOWNSTREAM DUCTWORK WERE COMPLETELY REPLACED. THE DOWNSTREAM DUCTWORK WAS RELINED WITH CEILCOTE.

ALSO DURING THE OUTAGE THE MODULE 401 INTERNALS WERE CLEANED AND SOME HOLES IN THE UPPER CONICAL REGION WERE REPAIRED.

THE SYSTEM CAME BACK ON LINE IN LATE MARCH, HOWEVER, BOILER NUMBER 3 WAS NOT IN SERVICE.

4/78 SYSTEM 720 720 5/78 SYSTEM 744 744

# ** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE APRIL-MAY PERIOD BOILER NUMBER 3 WAS STILL BEING OVERHAULED. FGD SYSTEM CONSTRUCTION WAS COMPLETED AND PRELIMINARY TESTING WITH THIOSORBIC LIME VERIFIED A SYSTEM SO2 REMOVAL EFFICIENCY OF 83%.

6/78	SYSTEM					720	720	
7/78	101	<b>5</b> 9.9	59.9	59.9	59.9			
	201	100.0	100.0	100.0	100.0			
	301	66.5	66.5	66.5	66.5			
	401	100.0	98.9	100.0	98.9			
	501	77.1	77.1	77.1	77.1			
	SYSTEM	100.0	100.0	100.0	100.0	744	744	744

## ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE 301 WAS PULLED OFF FOR A MAJOR CLEANING DURING THE JUNE-JULY PERIOD.

MIST ELIMINATOR PLUGGING WAS EXPERIENCED AS A RESULT OF LOW 2H.

THE CHRONIC INABILITY TO CONTROL CHEMISTRY (PH) IS DIRECTLY RELATED TO GRIT BUILD-UP IN THE LIME HANDLING AND SLURRY PREPARATION SYSTEM.

THE UTILITY IS CURRENTLY STUDYING WAYS TO TIGHTEN THE WATER BALANCE BY US-

DUQUESNE LIGHT: ELRAMA 1-4 (CONT.)

PERFORMANCE DATA										
PERIOD MODULE AVAILABILITY										
							HOURS			

ING THICKENER SUPERNATANT INTERMITTENTLY WITH CLEAR SERVICE WATER FOR THE MIST ELIMINATORS.

8/78	101	76.9	76.9	76.9	76.9			
	201	100.0	100.0	100.0	100.0			
	301	50.7	50.7	50.7	50.7			
	401	100.0	100.0	100.0	100.0			
	501	70.9	70.9	70.9	70.9			
	SYSTEM	99.6	100.0	99.6	99.6	744	744	741
9/78	101	72 <b>.1</b>	72.1	72.1	72.1			
	201	59.6	56.3	58.2	56.3			
	301	93.3	89.0	92.9	89. <b>0</b>			
	401	78.1	78.1	78.1	78.1			
	501	93.6	93.6	93.6	93.6			
	SYSTEM	99.2	100.0	98.7	97.3	720	720	700

## ** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE AUGUST-SEPTEMBER PERIOD THE UTILITY REPORTED THAT MODULES 301 AND 501 WERE TAKEN OFF LINE FOR CLEANING.

THE RUBBER LINING ON THREE FAN HOUSINGS REQUIRED REPAIR DURING AUGUST AND SEPTEMBER.

IT WAS NECESSARY TO SHUT DOWN THE LIME MIXING BASIN IN ORDER TO CLEAN OUT EXCESSIVE GRIT AND SOLIDS BUILD UP.

A PARTICLE EMISSION COMPLIANCE TEST WAS RUN IN DECEMBER WHICH SHOWED THE UNIT TO BE IN COMPLIANCE.

10/78	101	100.0	76.6	100.0	76.6			
	201	98.9	98 <b>.9</b>	98.9	98.9			
	301	100.0	100.0	100.0	100.0			
	401	80.5	80.5	80.5	80.5			
	501	78.6	78.6	78.6	78.6			
	SYSTEM	100.0	100.0	100.0	100.0	744	744	744
11/78	101	100.0	100.0	100.0	100.0			
	201	100.0	78.4	100.0	78.4			
	301	100.0	84.2	100.0	84.2			
	401	100.0	86.8	100.0	86.8			
	501	81.1	62.5	76.8	62.5			
	SYSTEM	100.0	100.0	100.0	100.0	720	720	720

^{**} PROBLEMS/SOLUTIONS/COMMENTS

THE PARTICLE EMISSION TEST RUN IN AUGUST SHOWED THAT THE UNIT MET STATE STANDARDS. THE SO2 TEST WILL HAVE TO BE RERUN BECAUSE OF SAMPLING ERRORS.

THE UTILITY REPORTED DURING THE OCTOBER-NOVEMBER PERIOD THAT IT HAS HAD SOME PROBLEMS WITH AN INSUFFICIENT LIME SUPPLY.

12/78	101	100.0	94.7	100.0	94.7			
	201	76.3	72.7	75.4	72.7			
	301	93.0	85.6	92.5	85.6			
	401	68.0	64.8	66.9	64.8			
	501	97. <b>9</b>	69.5	97.0	69.5			
	SYSTEM	100.0	100.0	100.0	96.8	744	744	720

DUQUESNE LIGHT: ELRAMA 1-4 (CONT.)

PERFORMANCE DATA									
PERIOD MODULE AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% REI	MOVAL	PER	BOILER	FGD	CAP.
,				502	PART.	HOURS	HOURS	HOURS	FACTOR

# ** PROBLEMS/SOLUTIONS/COMMENTS

DURING DECEMBER A SO2 EMISSION COMPLIANCE TEST WAS RUN AND THE UNIT WAS FOUND TO BE WITHIN THE ALLOWABLE STANDARD OF 0.6 LB/MM BTU.

1/79	101	44.7	39.8	41.9	39.8			
	201	100.0	95.2	100.0	95.2			
	301	67.8	60.2	65.3	60.2			
	401	100.0	100.0	100.0	100.0			
	501	100.0	100.0	100.0	100.0			
	SYSTEM	100.0	100.0	100.0	98.8	744	744	735

# ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY HAS STARTED HAULING SLUDGE OFF-SITE TO AN AREA ABOUT 10 MILES AWAY.

		ДР	4A 1 .					
2/79	101	100.0	100.0	100.0	100.0			
• •	201	90.2	90.2	90.2	90.2			
	301	14.1	14.1	14.1	14.1			
	401	97.8	97.3	97.8	97.3			
	501	100.0	100.0	100.0	100.0			
	SYSTEM	100.0	100.0	100.0	100.0	672	672	672
	3131611	100.0	100.0	100.0	100.0	072	072	072
3/79	101	98.9	95.4	98.8	95.4			
	201	100.0	91.0	100.0	91.0			
	301	77.7	73.8	76.8	73.8			
	401	54.5	39.2	46.3	39.2			
	501	70.4	65.9	69.0	65.9			
	SYSTEM	100.0	100.0	97.7	91.4	744	744	680
4/79		64.1	61.9	63.3	61.9			
	201	57.4	53.5	55.7	53.5			
	301	100.0	99.3	100.0	99.3			
	401	100.0	89.9	100.0	89.9			
	501	92.8	90.4	92.6	90.4			
	SYSTEM	100.0	95.6	100.0	95.6	720	720	688
5/79	101	100.0	100.0	100.0	100.0			
	201	97.8	97.8	97.8	97.8			
	301	100.0	83.1	100.0	83.1			
	401	100.0	100.0	100.0	100.0			
	501	51.6	21.4	30.6	21.4			
	SYSTEM	100.0	100.0	100.0	100.0	744	744	744
	0.0.0.	200.0	200.0	20000	20000			
6/79	101	100.0	100.0	100.0	100.0			
	201	98.5	58.5	97.5	58.5			
	301	93.3	40.0	85.7	40.0			
	401	100.0	100.0	100.0	100.0			
	501	100.0	100.0	100.0	100.0			
	SYSTEM	100.0	100.0	100.0	99.6	720	720	717
7.476								
7/79	101	100.0	81.0	100.0	81.0			
	201	100.0	94.8	100.0	94.8			
	301	86.0	86. <b>0</b>	86.0	86. <b>0</b>			
	401	100.0	99.3	100.0	99.3			
	501	40.7	40.7	40.7	40.7			
	SYSTEM	100.0	100.0	100.0	100.0	744	744	744
8/79	101	100.0	98.7	100.0	98.7			
	201	100.0	100.0	100.0	100.0			
	301	100.0	96.5	100.0	96.5			
	201	100.0	70.3	100.0	70.5			

DUQUESNE LIGHT: ELRAMA 1-4 (CONT.)

				PERFORMA	NCE DATA					
PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% REMOVAL SO2 PART.	PER HOURS	BOILER HOURS	FGD HOURS	CAP. FACTOR
	401	41.2	33.3	36.2	33.3					
	501	72.8		72.8	72.8					
	SYSTEM	-		100.0	100.0		744	744	744	
9/79	101	44.0	35.0	38.4	<b>3</b> 5. <b>0</b>					
	201	100.0	93.3	100.0	93.3					
	301	100.0	86. <del>6</del>	100.0	86. <b>6</b>					
	401	90.0	90.0	90.0	90.0					
	501	76.9	70.0	75.2	70.0					
	SYSTEM	100.0	93.8	100.0	93.8		720	720	675	
10/79	101	100.0	100.0	100.0	100.0					
	201	100.0	96.1	100.0	96.1					
	301	47.8	34.6	39.1	34.6					
	401	94.4	87.3	94.0	87.3					
	501	84.4	84.5	84.4	84.5					
	SYSTEM	100.0	100.0	100.0	100.0		744	744	744	
11/79	101	100.0	100.0	100.0	100.0					
	201	15.3	15.2	15.3	15.2					
	301	92.4	92.5	92.4	92.5					
	401	100.0	98.3	100.0	98.3					
	501	95.0	93.9	94.9	93.9					
	SYSTEM	100.0	100.0	100.0	100.0		720	720	720	
12/79	101	100.0	51.6	100.0	48.5					
	201	100.0	90.9	100.0	85.5					
	301	100.0	100.0	96.1	100.0					
	401	88.1	68.6	84.4	64.5					
	501	100.0	100.0	100.0	100.0					
	SYSTEM	100.0	100.0	100.0	98.7		744	700	734	

# ** PROBLEMS/SOLUTIONS/COMMENTS

THERE WERE NO SCRUBBER-RELATED OUTAGES DURING THE SEPTEMBER THROUGH DECEMBER PERIOD.

A NEW SO2 MONITOR, WHICH WAS INSTALLED IN OCTOBER, HAS PLUGGED ONLY ONCE SINCE INSTALLATION AND HAS REQUIRED ONLY FOUR HOURS OF MAINTENANCE PER WEEK.

1/80	101	95.8	91.2	94.8	75.2			
	201	87.1	100.0	87.1	87.1			
	301	84.6	100.0	84.6	84.6			
	401	86.4	55.6	77.1	45.8			
	501	100.0	100.0	100.0	100.0 -			
	SYSTEM	100.0	100.0	100.0	98.2	744	613	528
2/80	101	100.0	85.4	100.0	60.5			
	201	100.0	100.0	100.0	96.6			
	301	100.0	100.0	100.0	100.0			
	401	100.0	100.0	100.0	70.7			
	501	77.6	56.8	64.0	40.2			
	SYSTEM	100.0	100. <b>0</b>	100.0	92.0	<b>6</b> 96	493	427

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE NEW SO2 MONITOR INSTALLED LAST OCTOBER IS STILL OPERATING WELL AND HAS LOGGED SIX MONTHS OF OPERATION.

THE HIGH AVAILABILITIES ARE DUE TO THE 5TH MODULE BEING A TRUE SPARE. AS OF FEBRUARY 1980 AND ARE STILL OPERATING WITHOUT ANY MAJOR PROBLEMS.

THE TWO RUBBER LINED WORMEN RECYCLE PUMPS HAVE NOW LOGGED 14,000 HOURS

ERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILI	TY UTILIZATION				BOILER HOURS		
3/80				100.0					,		
	201	100.0	100.0	100.0	100.0						
	301	73.7	73.7	73.7	73.7						
	401	100.0	48.4	100.0	48.4						
	501	78.1	78.1	78.1	78.1						
	SYSTEM	100.0	100.0	100.0	100.0			744	744	595	
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
		Т	HE FGD SYSTE	M WAS AVAII	ABLE FOR OPERA	NOITA	THE EN	TIRE MO	ONTH OF	MARCH	•
4/80		40.3		40.0	40.0						
	201	72.3	72.3	72.3 87.3	72.3						
	301	87.3	87.3	87.3	87.3						
	401	100.0	100.0 100.0	100.0	100.0						
	501	100.0	100.0	100.0	100.0						
	SYSTEM	99.4						720	720	572	
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
		Т		IGHT HOURS	201 RECYCLE F OF OUTAGE TIME						
5/80	101	100.0	100 0	100 0	100 0						
<i>37</i> 00	201	40.1	37 1	78 2	37.1						
	301	94.1	27.1	38.2 93.8	89.0						
	401	77.1	71 2	88.0							
		90.3 96.8	71.2 96.8	96.8	96.8						
	501 SYSTEM	100.0			98.5			744	744	586	
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
		D	URING MAY TH	HE FGD SYST	EM WAS AVAILAB!	LE FOR	OPERA	TION T	HE ENTI	RE MON	гн.
6/80	101	100.0	100.0	100.0	100.0						
	201	100.0	97.8	100.0							
	301		96.7								
	401	.0	.0	.0							
	501	100.0	100.0	100.0	100.0						
		100.0		99.7				720	720	710	61.6
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
		_			WAS CLEANED AND						
					SINCE START UP NEEDED RELINED		UXIMAT	ELT 1/	,000 UP	ERAIIN	3
		-	OURING JUNE 1	NO FGD-RELA	TED PROBLEMS O	CCURRE	и ио о	ODULES	101, 2	01, 30	1 OR
7/80	101	100.0	64.9	100.0	64.9						
	201	100.0	91.1	100.0	91.1						
	301	98.5	85.6	98.3	85.6						
	401	75.8	75.8	75.8	75.8						
	501	35.5	12.9	16.7	12.9						
	SYSTEM		82.6	97.7	82.6			744	744	615	66.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
		Т	HE RELINING	OF MODULE	401 CONTINUED :	INTO P	ART OF	JULY.			

8/80 101 30.9 21.2 23.5 21.2

DUQUESNE LIGHT: ELRAMA 1-4 (CONT.)

			PFRF0RMAI	NCE BATA						
	AVAILABILITY				% RE	MOVAL	PER	BOILER HOURS	FGD	CAP.
 201	100.0	94.8	100.0	94.8						
301	100.0	93.3	100. <b>0</b>	93.3						
401	99.1	99.1	99.1	99.1						
501	83.9	82.5	83.7	82.5						
SYSTEM	100.0	97.7	100.0	97.7			744	744	727	65.0

# ** PROBLEMS/SOLUTIONS/COMMENTS

THE RELINING WITH CEILCOTE ON MODULE 501 COMMENCED IN JULY AND CONTINUED FOR APPROXIMATELY 120 HOURS IN AUGUST.

THE RELINING OF MODULE 101 WITH CEILCOTE STARTED IN AUGUST ACCOUNTING FOR THE LOW AVAILABILITY DURING THE MONTH.

9/80	101	59.7	59.7	59.7	59.7				
	201	39.0	22.8	27.2	22.8				
	301	100.0	100.0	100.0	96. <b>0</b>				
	401	100.0	100.0	100.0	100.0				
	501	100.0	99.2	100.0	99.2				
	SYSTEM	99.7	95.4	96.8	94.4	720	720	680	64.5
10/80	101	97.9	95.8	97.8	95.8				
	201	32.4	23.3	25.6	23.3				
	301	98.5	98.5	98.5	98.5				
	401	90.5	72.7	88.3	72.7				
	501	98.5	96.5	98.4	96.5				
	SYSTEM	100.0	96.8	100.0	96.8	744	744	720	75.1
11/80	101	68.8	68.8	68.8	68.8				
	201	96.4	96.4	96.4	96.4				
	301	62.6	59.3	61.4	59.3				
	401	93.8	93.8	93.8	93.8				
	501	77.2	77.2	77.2	77.2				
	SYSTEM	99.8	98.9	99.4	98.9	720	720	711	79.3

## ** PROBLEMS/SOLUTIONS/COMMENTS

DURING SEPTEMBER-NOVEMBER THE LINERS IN MODULES 101, 201 AND 301 WERE REPLACED.

DURING NOVEMBER THE RUBBER LINER IN THE FAN HOUSING OF MODULE 101 WAS COATED WITH URETHANE.

THE UTILITY REPORTED THAT THE WORMAN RECYCLE PUMPS HAVE NOW ATTAINED 20,000 HOURS OF OPERATION WITHOUT REPAIRS.

12/80	101 201 301 401 501	73.0 100.0 98.9 48.4 94.9	55.1 81.3 94.6 48.4 93.4	67.1 100.0 98.9 48.4 94.8	55.1 81.3 94.6 48.4 93.4				
	SYSTEM	100.0	93.3	100.0	93.3	744	744	694	54.8
1/81	101 201 301 401 501 SYSTEM	100.0 92.5 100.0 32.2 88.2 100.0	100.0 51.1 96.6 .0 51.1 74.7	100.0 87.1 100.0 .0 81.2 92.1	100.0 51.1 96.6 .0 51.1 74.7	744	744	554	41.0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING DECEMBER AND JANUARY.

2/81	101	92.1	51.6	73.5	51.6				
	201	99.1	86.5	88.2	86. <b>5</b>				
	301	98.9	93.2	98.9	93.2				
	401	3.6	3.6	3.6	3.6				
	501	95.2	93.6	95.2	93.6				
	SYSTEM	97.2	82.1	89.9	82.1	672	672	552	33.6

#### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING FEBRUARY THE RUBBER LININGS ON THE FAN HOUSINGS OF MODULES 201 AND 301 WERE REPLACED WITH INCONEL 825.

3/81	101	59.8	38.7	49.1	38.7				
	201	59.1	59.1	59.1	59.1				
	301	53.6	53.6	53.6	53.6				
	401	21.1	21.1	21.1	21.1				
	501	59.9	<b>5</b> 8. <b>9</b>	59.5	58.9				
	SYSTEM	63.4	57.9	60.6	57.9	744	744	431	41.4

## ** PROBLEMS/SOLUTIONS/COMMENTS

UTILITY REPORTED THAT THE LOW BOILER CAPACITY FACTOR FOR THE MONTH OF MARCH WAS DUE TO THE COAL STRIKE (BOILERS WERE RUN AT REDUCED LOAD TO CONSERVE FUEL). GENERAL CLEANING WAS PERFORMED ON BOTH BOILERS AND FGD SYSTEM DURING THE MONTH.

THE FGD SYSTEM WAS DOWN FOR 10 DAYS TO REPAIR THE DUCTWORK AND EXPANSION JOINT LOCATED AT THE STACK. DURING THE OUTAGE, THE STACK, DAMPERS, AND REMAINING EXPANSION JOINTS WERE INSPECTED. THE STACK INSPECTION SHOWED MINOR DETERIORATION OF THE STACK FLUE.

4/81	101	88.1	76.9	86.6	76.9				
	201	72.3	46.2	62.5	46.2				
	301	90.0	82.6	89.2	82.6				
	401	86.7	85.6	86.6	85.6				
	501	94.2	82.3	93.4	82.3				
	SYSTEM	100.0	93.4	100.0	93.4	720	719	672	68.6

## ** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE MONTH OF APRIL.

THE RUBBER COATED FAN HOUSING ON NUMBER 401 ID FAN WAS SPRAYED WITH A POLYURETHANE COATING TO PROTECT AGAINST CORROSION/EROSION EFFECTS.

SODIUM THIOSULFATE ADDITION WAS INITIATED IN APRIL TO AID AGAINST SCALING (HIGH EXCESS AIR PROBLEMS WHEN BOILERS RUN AT REDUCED LOADS).

5/81	101	100.0	96.7	100.0	96.7				
	201	.0	. 0	.0	.0				
	301	100.0	100.0	100.0	100.0				
	401	100.0	67.0	100.0	67.0				
	501	<b>8</b> 8.7	50.2	81.7	50.2				
	SYSTEM	97.2	78.5	95.4	78.5	744	744	584	46.7

DUQUESNE LIGHT: ELRAMA 1-4 (CONT.)

EKTOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% RE SO2	MOVAL PART.	PER HOURS	BOILER HOURS	FGD HOURS	CAP. FACTOR
			~~~~								
	** PROB	SLEMS/SOLUTIO	NS/COMMENTS								
		-			HE INGERSOLL LINED WORMAN			E PUMPS	ON MOI	OULE 20	01
6/81	101	95.4	92.6	97.1	92.6						
J. J.	201	95.4 61.7	61.7								
	301	93.3	86.0	92.8	86. 0						
	401	88.3	86.0 76.7	86.8	76.7						
			41.5	53.5	41.5						
	SYSTEM	63.9 100.0	89.6	98.0	89.6			720	72 0	645	58.0
7/81	101	98.9	86.0	98.8	86.0						
	201	100.0	98. 9	100.0	98.9						
	301	.0	.0	.0	.0						
	401	98.4	93.3 100.0	98.2 100.0	93.3 10 0. 0						
	501	100.0									
	SYSTEM	99.3	94.6	99.3	94.6			744	744	704	67.0
	** PROE	BLEMS/SOLUTIO	NS/COMMENTS								
		D	URING JULY, I	MODULE 301 H	IAS OUT OF SER	VICE	FOR GEI	NERAL (CLEANING	S AND I	FOR TH
		I	NSTALLATION (OF POLYURETH	ANE IN THE FA	M HOU	SING.				
8/81	101	97.3	90.5	97.3	90.5						
	201		58.5								
	301	0	.0	.0	. 0						
	401	97.7	95.6		95.6	•					
	501	97.4	80.9	96.9	80.9				_		
	SYSTEM	97.8	81.4	97.5	81.4			744	744	606	43.0
	** PROB	BLEMS/SOLUTIO	NS/COMMENTS								
		М	ODULE 301 RE	MAINED DOWN	DURING AUGUST	FOR	MAINTE	NANCE /	AND CLE	ANING.	
9/81	101	100.0	68.2	100.0	68.2						
	201	100.0	98.3	100.0	98.3						
	301	.0	. 0		. 0						
	401	100.0	87.2 51.0	100.0 100.0	87.2						
	501	100.0	51.0	100.0	51.0						
	SYSTEM	100.0	76.2		76.2			720	720	549	39.8
	** PROB	BLEMS/SOLUTIO	NS/COMMENTS								
	** PROB	D			01 WAS OUT OF	SERV	ICE FO	R CLEA	HING AM	D TO R	EPLACE
.0/81	101	D	URING SEPTEM		001 WAS OUT OF	SERV	ICE FO	R CLEA!	NING AN	D TO R	EPLACE
0/81	101 201	D T	URING SEPTEM HE RECYCLE P	UMP.		SERV	ICE FO	R CLEA!	HING AN	D TO R	EPLACE
.0/81	101 201 301	D T 85.6	URING SEPTEM HE RECYCLE P 62.1	UMP. 81.2	62.1	SERV	ICE FO	R CLEA	HING AN	D TO R	EPLACE
0/81	101 201 301 401	85.6 100.0	URING SEPTEM HE RECYCLE P 62.1 95.3	UMP. 81.2 100.0	62.1 95.3	· SERV	ICE FO	R CLEA	VING AN	D TO R	EPLACE
.0/81	101 201 301 401 501	85.6 100.0 .0 96.0 100.0	URING SEPTEM HE RECYCLE P 62.1 95.3 .0	81.2 100.0 .0	62.1 95.3 .0	SERV	ICE FO	R CLEAI	NA DNIV	D TO R	EPLACE
.0/81	101 201 301 401	85.6 100.0 .0 96.0 100.0	URING SEPTEM HE RECYCLE P 62.1 95.3 .0 94.0	81.2 100.0 .0 95.8	62.1 95.3 .0 94.0	SERV	ICE FO	R CLEAI			45.0

DURING OCTOBER THE SO2 MONITORS WERE CERTIFIED. TO DATE, THE MONITORS HAVE AN EXCELLENT PERFORMANCE RECORD.

THE UTILITY CONTINUES TO ADD SODIUM THIOSULFATE TO CONTROL SCALE BELIEVED TO BE CAUSED BY LOAD FLUCTUATIONS.

11/81 101 100.0 69.0 100.0 69.0

720

DUQUESNE LIGHT: ELRAMA 1-4 (CONT.)

9/82 SYSTEM

PERIOD	MODULE	AVAILABILITY	OPERABILITY		UTILIZATION	S02	PART.	HOURS	HOURS	HOURS	
	201	100.0	100.0								
	301	.0	.0	.0 100.0	.0						
	401	100.0	84.8	100.0	.84.8						
	501	100.0	55.0	100.0	55.0						
	SYSTEM	100.0	77.2	100.0	77.2			720	720	556	48.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			URING NOVEMB	ER, THE MODU	JLE 301 RECYCL	.E PUMI	PS WER	E REPL	ACED WI	TH RUB!	BER
12/81	101	100.0	30.3	100.0	30.3						
,,,,,,	201	94.5	80.2	93.5	00.0						
	301	94.5 91.9	90.7	93.5 91.7	90.7						
	401	13.5	13.5	13.5	13.5						
	501	100.0	13.5 26.2	100.0	24.2						
	SYSTEM	99.9	60.2	99.7	60.2			744	744	448	46.0
		BLEMS/SOLUTIO		1							
	, 1100			FR. THE UTT!	ITY REPORTED	FYPFD.	FNCTN	s PROBI	FMS UT	TH THE	
					LOAD FLUCTUAT			G PRODE	LENS AI	,,, ,,,,	
1/82	101	60.0	43.2	51.9							
	201	96.6	94.0	96.5	94. 0						
	301	100.0	94.4	79.3 90.8	94.4						
	401	90.8	90.8	90.8	90.8						
	501	53.7	49.6	51.7	49.6						
	SYSTEM	100.0	49.6 94.4	79.3	94.4			744	744	702	73.0
2/82	101	.0	.0	.0 79.4 96.2	.0						
	201	79.6 96.3		79.4	78.5 93.9						
	301	96.3	78.5 93.9	96.2	93.9						
	401	100.0	82.6 81.3	100.0	82.6						
	501	91.4	81.3	90.4	81.3						
	SYSTEM		84.1					672	672	565	59.0
3/82	101	. 0	. 0	. 0	. 0						
	201	.0 98.2	97.1	.0 98.2	.0 97.1						
	301	95.8	85.2	95.4	85.2						
	401	91.6	90.8	91.5	90.8						
		100.0	90.0	100.0							
	SYSTEM			76.5	92.8			744	744	691	67.0
	** PROE	SLEMS/SOLUTIO	NS/COMMENTS								
					OF 1982, THE	MODUL	E 101	RECYCLI	E PUMPS	WERE	
		R	PEPLACED WITH	RUBBER LINE	D PUMPS.						
	SYSTEM							720			
5/82	SYSTEM							744			
6/82	SYSTEM							720			
	** PROS	BLEMS/SOLUTIO	NS/COMMENTS								
						ON OF	THE D	ECYCLE	DIRADO	TO DIE	RED
			URING THE SE			LUN UF	וחב א	ECICLE	PUNPS	TO ROB	DER
7/82	SYSTEM					LON OF	וחב א	744		IU ROB	DLK

DUQUESNE LIGHT: ELRAMA 1-4 (CONT.)

*****		PERFORM	ANCE DATA						
		TY OPERABILITY RELIABILIT		% REN SO2	10VAL PART.	PER HOURS	BOILER HOURS	FGD HOURS	CAP. FACTOR
			~~~~~~						
10/82	SYSTEM					744			
11/82	SYSTEM					720			
12/82	SYSTEM					744			
1/83	SYSTEM					744			
2/83	SYSTEM					672			
3/83	SYSTEM					744			
	** PROBLEMS/SOLUT	IONS/COMMENTS							
		INFORMATION WAS UNAVAILA	BLE FOR THE PE	RIOD C	OF JUL'	Y 1982	THROUG	H MARCH	1983.
4/83	SYSTEM					720			
5/83	SYSTEM					744			
6/83	SYSTEM					720			
	** PROBLEMS/SOLUT	IONS/COMMENTS							
		INFORMATION WAS UNAVAILA	BLE FOR THE PE	RIOD C	OF JUL	Y 1982	THROUG	JUNE	1983.
7/83	SYSTEM					744			
8/83	SYSTEM					744			
9/83	SYSTEM					720			
	** PROBLEMS/SOLUT	IONS/COMMENTS							
		THE UTILITY REPORTED COM AND AUGUST 1983.	PLIANCE WITH S	STACK E	EMISSI	ON TES	TS CONDI	JCTED :	IN JULY
10/83	SYSTEM					744			
11/83	SYSTEM					720			
	** PROBLEMS/SOLUT	IONS/COMMENTS							
		THE UTILITY REPORTED A TITIME DAMPER AND DUCTWORK				NOVEMB:	ER, DUR	ING WH	ICH
12/83	SYSTEM					744			
	** PROBLEMS/SOLUT	IONS/COMMENTS							
		THE UTILITY REPORTED INSTITUTE TO THE USE OF ADDITIVES IN	UARTER. THE 7	750 ACE	FM MODI	ULE WI	LL BE U	ELRAM SED TO	A STA- TEST
1/84	SYSTEM					744			
2/84	SYSTEM					696			
3/84	SYSTEM					744			
4/84	SYSTEM					720			
5/84	SYSTEM					744			

DUQUESNE LIGHT: ELRAMA 1-4 (CONT.)

			PERFORMA	NCE DATA				 		
		LITY OPERABILITY			% REN	10VAL	PER	FGD	CAP.	
6/84	SYSTEM						720			
7/84	SYSTEM						744			
8/84	SYSTEM						744			
9/84	SYSTEM						720			

## ** PROBLEMS/SOLUTIONS/COMMENTS

OVERALL FGD SYSTEM AVAILABILITY FOR THE FIRST THREE QUARTERS OF 1984 WAS ESTIMATED AT 90%.

THE UTILITY REPORTED THAT DUE TO A TIGHTENING OF THE WATER LOOP, IT IS NO LONGER NECESSARY TO SPIKE THE THIOSORBIC LIME WITH DOLOMITIC LIME. THE MAGNESIUM OXIDE CONTENT OF THE THISORBIC LIME IS SUFFICENT FOR OPERATIONS.

THE UTILITY IS NOW DIVERTING INDUCED DRAFT FAN SPRAY WATER TO AN ASH POND INSTEAD OF RECYCLING TO THE ABSORBERS. LIME CONSMPTION HAS IMPROVED SINCE THE HIGHLY ACIDIC SPRAY WATER IS NO LONGER INTRODUCED IN THE SYSTEM.

THE UTILITY REPORTED A THREE WEEK SCHEDULED ANNUAL OUTAGE IN THE FIRST THREE QUARTERS OF 1984. DURING THIS TIME REPAIRS WERE MADE TO DUCTWORK AND DAMPERS. MIST ELIMINATOR TURN VANES WERE ALSO REPLACED.

THE 1000 CFM PILOT SCRUBBER LOANED TO THE UTILITY BY DRAVO IS NOW IN OPERATION. THIS PILOT SCRUBBER IS USED TO TEST VARIOUS ADDITIVES TO THE LIME PROCESS SUCH AS SODIUM THIOSULFATE AND OTHER ORGANIC ADDITIVES.

# SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

-----DUQUESNE LIGHT COMPANY NAME PHILLIPS PLANT NAME 1-6 UNIT NUMBER SOUTH HEIGHTS CITY PENNSYLVANIA STATE С REGULATORY CLASSIFICATION 34. ( .080 LB/MMBTU) 258. ( .600 LB/MMBTU) ****** (****** LB/MMBTU) PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J 387 NET PLANT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW
NET UNIT GENERATING CAPACITY W/FGD - MW
NET UNIT GENERATING CAPACITY WO/FGD - MW 408 373 387 NET UNIT GENERATING CAPACITY WO/FGD - MW EQUIVALENT SCRUBBED CAPACITY - MW 408 ** UNIT DATA - BOILER AND STACK FOSTER WHEELER BOILER SUPPLIER BOILER TYPE PULVERIZED COAL CYCLING
1047.62 (2220000 ACFM)
183.3 (362 F)
104. (340 FT)
CONCRETE BOILER SERVICE LOAD DESIGN BOILER FLUE GAS FLOW - CU.M/S
BOILER FLUE GAS TEMPERATURE - C STACK HEIGHT - M STACK SHELL STACK TOP DIAMETER - M 7.9 ( 26.0 FT) ** FUEL DATA FUEL TYPE COAL BITUMINOUS FUEL GRADE AVERAGE HEAT CONTENT - J/G 26907. ( 11568 BTU/LB) RANGE HEAT CONTENT - BTU/LB 11500-12500 AVERAGE ASH CONTENT - % 16.80 14.0-18.3 RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - % 5.93 RANGE MOISTURE CONTENT - % 4.3-7.1 AVERAGE SULFUR CONTENT - % 2.05 1.5-2.9 .04 .03-.05 RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - % *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER 6 NUMBER OF SPARES 0 MULTICLONE SUPPLIER RESEARCH-COTTRELL 174.6 ( 370000 ACFM) 183.3 ( 362 F) .1 ( 1. IN-H20) INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE - C PRESSURE DROP - KPA ** ESP NUMBER 6 NUMBER OF SPARES ۵ TYPE COLD SIDE SUPPLIER
INLET FLUE GAS CAPACITY - CU.M/S RESEARCH-COTTRELL 174.6 ( 370000 ACFM) 183.3 ( 362 F) .1 ( 1. IN-H20) 70.0 INLET FLUE GAS TEMPERATURE - C PRESSURE DROP - KPA PARTICLE REMOVAL EFFICENCY - % ** PARTICLE SCRUBBER NUMBER GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A LINER GENERIC MATERIAL

ORGANIC

DUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)

## *** FGD SYSTEM

```
** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                               THROWAWAY PRODUCT
                                               WET SCRUBBING
   SO2 REMOVAL MODE
   PROCESS TYPE
                                               LIME
   PROCESS ADDITIVES
                                               MAGNESIUM OXIDE, SODIUM
   SYSTEM SUPPLIER
                                               GE ENVIRONMENTAL SERVICES
   A-E FIRM
                                               GIBBS & HILL
   DEVELOPMENT LEVEL
                                               FULL SCALE
   NEW/RETROFIT
                                               RETROFIT
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.00
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                  83.00
   ENERGY CONSUMPTION - %
   CURRENT STATUS
                                                1
   COMMERCIAL START-UP
                                                6/74
   INITIAL START-UP
                                                7/73
   CONTRACT AWARDED
                                                7/71
** DESIGN AND OPERATING PARAMETERS
   DESIGN COAL SULFER CONTENT - %
                                                  2.30
   DESIGN COAL HEAT CONTENT - J/G
                                               25586.0
                                                              ( 11000 BTU/LB)
   DESIGN COAL ASH CONTENT - %
                                                  21.00
   DESIGN MOISTURE CONTENT - %
                                                   7.00
   DESIGN CHLORIDE CONTENT - %
                                                    .10
   SPACE REQUIREMENTS - SQ M
                                               24246.9
                                                              ( 261000 SQ FT)
   OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                 140.0
** QUENCHER/PRESATURATOR
                                               NONE
   TYPE
** ABSORBER
   NUMBER
                                                4
   NUMBER OF SPARES
                                                0
   GENERIC TYPE
                                               VENTURI TOWER
   SPECIFIC TYPE
                                               VARIABLE-THROAT/SIDE-MOVABLE BLADES
   TRADE NAME/COMMON TYPE
                                               N/A
   SUPPLIER
                                               GE ENVIRONMENTAL SERVICES
   DIMENSIONS - FT
                                               40.0 X 66.0
    SHELL GENERIC MATERIAL
                                               CARBON STEEL
    SHELL SPECIFIC MATERIAL
                                               AISI 1110
   SHELL MATERIAL TRADE NAME/COMMON TYPE
                                               N/A
    LINER GENERIC MATERIAL
                                               DRGANIC
    LINER SPECIFIC MATERIAL
                                               MAT-REINFORCED EPOXY; GLASS FLAKE-FILLED POLYEST
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                               COROLINE 505AR; FLAKELINE 103
   GAS CONTACTING DEVICE TYPE
                                               VARIABLE THROAT VENTURI
   NUMBER OF CONTACTING ZONES
                                                1
    LIQUID RECIRCULATION RATE - LITER/S
                                                1008.
                                                              (16000 GPM)
    L/G RATIO - L/CU.M
                                                   3.9
                                                              ( 29.1 GAL/1000 ACF)
                                                              ( 8.0 IN-H20)
   GAS-SIDE PRESSURE DROP - KPA
                                                   2.0
                                                          (150.0 FT/S)
( 550000 ACFM)
   SUPERFICAL GAS VELOCITY - M/SEC
                                                 45.7
                                                 259.54
    INLET GAS FLOW - CU. M/S
    INLET GAS TEMPERATURE - C
                                                 183.3
                                                              ( 362 F)
    502 REMOVAL EFFICIENCY - X
                                                  84.0
   PARTICLE REMOVAL EFFICENCY - %
                                                  99.0
** MIST ELIMINATOR
                                              PRIMARY COLLECTOR [EXTERNAL]
   PRE-MIST ELIMINATOR/MIST ELIMINATOR
   NUMBER PER SYSTEM
                                               3
   NUMBER OF SPARES PER SYSTEM
                                               0
   NUMBER PER MODULE
                                                1
   GENERIC TYPE
                                               IMPINGEMENT
   SPECIFIC TYPE
                                               BAFFLE
                                               CLOSED VANE
   TRADE NAME/COMMON TYPE
                                               HEIL
   MANUFACTURER
                                               HORIZONTAL
   CONFIGURATION
   NUMBER OF STAGES
                                                   1
   NUMBER OF PASSES PER STAGE
                                                   4
   FREEBOARD DISTANCE - M
                                                   5.79
                                                              (19.0 FT)
   DISTANCE BETWEEN VANES - CM
                                                   5.1
                                                              ( 2.00 IN)
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DUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)
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90 VANE ANGLES - DEGREES 1.0 ( 4.0 IN-H20) PRESSURE DROP - KPA SUPERFICAL GAS VELOCITY - M/S 3.0 ( 10.0 FT/S) CONSTRUCTION MATERIAL GENERIC TYPE ORGANIC FIBER-REINFORCED POLYESTER CONSTRUCTION MATERIAL SPECIFIC TYPE THICKENER OVERFLOW WASH WATER SOURCE CONTINUOUS WASH FREQUENCY ** REHEATER 2 NUMBER DIRECT COMBUSTION GENERIC TYPE IN-LINE BURNER SPECIFIC TYPE TRADE NAME/COMMON TYPE OIL 16.7 30 F) TEMPERATURE INCREASE - C CONSTRUCTION MATERIAL GENERIC TYPE NR CONSTRUCTION MATERIAL SPECIFIC TYPE NR ** FANS 4 NUMBER NUMBER OF SPARES 0 DESIGN CENTRIFUGAL GREEN FUEL ECONOMIZER SUPPLIER **FUNCTION** BOOSTER INDUCED DRAFT **APPLICATION** SERVICE WET FLUE GAS FLOW RATE - CU.M/S 188.76 ( 400000 ACFM) FLUE GAS TEMPERATURE - C 51.7 ( 125 F) PRESSURE DROP - KPA 5.2 (17.0 IN-H20) CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL; HIGH ALLOY; HIGH ALLOY; STAINLESS ** DAMPERS NUMBER FUNCTION SHUT-OFF GENERIC TYPE BUTTERFLY SPECIFIC TYPE N/A MODULATION OPEN/CLOSED SEAL AIR FLOW - CU. M/S .00 1 0 ACFM) CONSTRUCTION MATERIAL GENERIC TYPE LINED CARBON STEEL CONSTRUCTION MATERIAL SPECIFIC TYPE AISI 1110 LINER GENERIC MATERIAL TYPE STAINLESS STEEL LINER SPECIFIC MATERIAL TYPE AUSTENITIC ** DAMPERS NUMBER 4 SHUT-OFF FUNCTION GENERIC TYPE LOUVER SPECIFIC TYPE PARALLEL BLADE MULTILOUVER MODULATION OPEN/CLOSED SEAL AIR FLOW - CU. M/S .00 0 ACFM) CONSTRUCTION MATERIAL GENERIC TYPE STAINLESS STEEL CONSTRUCTION MATERIAL SPECIFIC TYPE **AUSTENITIC** LINER GENERIC MATERIAL TYPE STAINLESS STEEL LINER SPECIFIC MATERIAL TYPE AUSTENITIC ** DAMPERS NUMBER 4 FUNCTION SHUT-OFF GENERIC TYPE LOUVER SPECIFIC TYPE PARALLEL BLADE MULTILOUVER MODULATION OPEN/CLOSED SEAL AIR FLOW - CU. M/S .00 0 ACFM) CONSTRUCTION MATERIAL GENERIC TYPE STAINLESS STEEL CONSTRUCTION MATERIAL SPECIFIC TYPE **AUSTENITIC** LINER GENERIC MATERIAL TYPE NR LINER SPECIFIC MATERIAL TYPE NR ** DUCTWORK LOCATION SCRUBBER INLET CONFIGURATION RECTANGULAR DIMENSIONS NΑ SHELL GENERIC MATERIAL TYPE CARBON STEEL

## DUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)

SHELL SPECIFIC MATERIAL TYPE **AISI 1110** LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A

## ** DUCTWORK

LOCATION CONFIGURATION DIMENSIONS SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE

RECTANGULAR NA CARBON STEEL AISI 1110

SCRUBBER OUTLET

ORGANIC GLASS FLAKE-FILLED POLYESTER

( 4 TPH)

#### ** REAGENT PREPARATION EQUIPMENT

FUNCTION SLAKER DEVICE SLAKER DEVICE TYPE PASTE MANUFACTURER WALLACE & TIERNAN NUMBER NUMBER OF SPARES FULL LOAD DRY FEED CAPACITY - M.TONS/HR 3.6 PRODUCT QUALITY - % SOLIDS 22.5

** TANKS

SERVICE NUMBER ABSORBER RECYCLE 4 REAGENT PREP PRODUCT 1 THICKENER OVERFLOW 1 SLUDGE STABILIZATION 1

#### ** PUMPS

SERVICE NUMBER SCRUBBER/ABSORBER RECIRCULATION 8 THICKENER OVERFLOW 6 THICKENER UNDERFLOW 1 SLURRY FEED 5 MAKEUP WATER 1

# ** SOLIDS CONCENTRATING/DEWATERING

DEVICE NUMBER NUMBER OF SPARES CONFIGURATION DIMENSIONS - FT CAPACITY FEED STREAM SOURCE FEED STREAM CHARACTERISTICS OUTLET STREAM CHARACTERISTICS OVERFLOW STREAM CHARACTERISTICS OUTLET STREAM DISPOSITION OVERFLOW STREAM DISPOSITION

# VACUUM FILTER

2 1 CIRCULAR 12(DIA)X16 150 LB/HR/SQ FT OF CLOTH THICKENER UNDERFLOW 30-35% SOLIDS 50% SOLIDS <0.1% SOLIDS SLUDGE TREATMENT THICKENER UNDERFLOW TANK

## ** SOLIDS CONCENTRATING/DEWATERING

DEVICE NUMBER NUMBER OF SPARES CONFIGURATION DIMENSIONS FT SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE FEED STREAM SOURCE FEED STREAM CHARACTERISTICS OUTLET STREAM CHARACTERISTICS OUTLET STREAM DISPOSITION OVERFLOW STREAM DISPOSITION

# THICKENER

3 1 CIRCULAR 75.0 DIA CARBON STEEL AISI 1110 ORGANIC GLASS FLAKE-FILLED POLYESTER ABSORBER BLEED 5% SOLIDS 30-35% SOLIDS VACUUM FILTER ME WASH

DUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)

***	SLUDGE	A7 F
	MOISTURE CONTENT - % TOTAL FREE WATER	27.5 4.0
	% CASO3 - DRY	10.0
	% CASO4 - DRY % ASH - DRY	50.0
	% A311 - DK1	
××	TREATMENT	•
	METHOD	FIXATION
	DEVICE	PUG MILL
	PROPRIETARY PROCESS	CONVERSION SYSTEMS [POZ-O-TEC] 34.6 ( 550 GPM)
	INLET FLOW RATE - LITER/S INLET QUALITY - %	50.0
	INCE! GOACIII "	
**	DISPOSAL	
	NATURE	INTERIM
	TYPE	CONCRETE PAD FOR ON-SITE CURING
	LOCATION SITE TRANSPORTATION METHOD	CN-SITE PIPELINE
	SITE TREATMENT	N/A
**	DISPOSAL	
	NATURE	FINAL
	TYPE	LANDFILL OFF-SITE
	LOCATION SITE TRANSPORTATION METHOD	TRUCK
	SITE TREATMENT	CLAY LINING
	SITE SERVICE LIFE - YRS	10
**	PROCESS CONTROL AND INSTRUMENTATION	CLIMBY RECEDEN ATTON CTREAM
	PROCESS STREAM CHEMICAL PARAMETERS	SLURRY RECIRCULATION STREAM PH
	PHYSICAL VARIABLES	FLOW
	CONTROL LEVELS	PH SET 7.7
	MONITOR TYPE	UNIVERSAL UNILOC
	MONITOR LOCATION	TANGENTIAL NOZZLE AT INLET TO ABSORBER
	PROCESS CONTROL MANNER	AUTOMATIC
	PROCESS CHEMISTRY MODE	FEEDBACK
××	WATER BALANCE	
	WATER LOOP TYPE	OPEN
	EVAPORATION WATER LOSS - LITER/S	13.9 ( 220 GPM)
	SLUDGE HYDRATION WATER LOSS - LITER/S SLUDGE INTERSTITIAL WATER LOSS - LITERS/S	1.9 ( 30 GPM) 3.1 ( 50 GPM)
	POND SEEPAGE/RUNOFF WATER LOSS - LITERS/S	
	RECEIVING WATER STREAM	OHIO RIVER
	MAKEUP WATER ADDITION - LITERS/S	22.0 ( 350 GPM)
	SOURCE OF MAKEUP WATER	RIVER
**	CHEMICALS AND CONSUMPTION	
	FUNCTION	ABSORBENT
	NAME	MAGNESIUM-MODIFIED LIME
	PRINCIPAL CONSTITUENT	CAO, MGD
	SOURCE/SUPPLIER	DRAVO
	CONSUMPTION UTILIZATION %	120 TPD
	POINT OF ADDITION	85.0 Slaker
	7 51777 57 255212577	SEARER
**	FGD SPARE CAPACITY INDICES	
	ABSORBER - X	.0
	MIST ELIMINATOR %	.0
	FAN - % SLAKER - %	.0
	EFFLUENT HOLD TANK - %	.0 .0
	RECIRCULATION PUMP - %	.0
	THICKENER - Z	50.0
	VACUUM FILTER - %	100.0

DUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)

<b>+</b>	FGD SPARE COMPONENT INDICES	
	ABSORBER	.0
	MIST ELIMINATOR	.0
	FAN	.0
	SLAKER	.0
	EFFLUENT HOLD TANK	.0
	RECIRCULATION PUMP	.0
	THICKENER	.5
	VACUUM FILTER	1.0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

# 0/73 SYSTEM

## ** PROBLEMS/SOLUTIONS/COMMENTS

DETERMINATION OF THE AVAILABILITY OF THE PHILLIPS SYSTEM HAS BEEN DIFFICULT. UNTIL ALL BOILERS WERE CONNECTED TO THE SCRUBBERS, THERE WAS AT LEAST ONE SPARE TRAIN AND AS MUCH AS 100% SPARE SCRUBBER CAPACITY. THEREFORE HAVING A TRAIN OUT OF SERVICE FOR MAINTENANCE DID NOT REDUCE THE CAPABILITY OF THE SCRUBBER SYSTEM. UNTIL ALL SIX BOILERS WERE CONNECTED, MEANINGFUL AVAILABILITY FACTORS COULD NOT BE COMPUTED. ON MARCH 17, 1975, THE SIXTH BOILER WAS CONNECTED, AND ALL FOUR SCRUBBER TRAINSWERE REQUIRED TO BE IN SERVICE. OPERATION IN THAT MODE CONTINUED UNTIL AUGUST 4, 1975, WHEN THE NO. 6 BOILER WAS REMOVED FROM THE SCRUBBER SYSTEM BECAUSE THE PH LEVEL COULD NOT BE MAINTAINED AND DEPOSITS BECAME UNMANAGEABLE TO THE POINT THAT SCRUBBER OUTAGES WERE REDUCING GENERATING CAPABILITY OF THE STATION.

7/73 SYSTEM 81.0 31.2 744 232

## ** PROBLEMS/SOLUTIONS/COMMENTS

## SCRUBBING OPERATIONS BEGAN DURING JULY.

8/73	SYSTEM	744
9/73	SYSTEM	720
10/73	SYSTEM	744
11/73	SYSTEM	720
12/73	SYSTEM	744
1/74	SYSTEM	744
2/74	SYSTEM	672
3/74	SYSTEM	744

## ** PROBLEMS/SOLUTIONS/COMMENTS

STARTUP OF A PORTION OF THE PHILLIPS SCRUBBER SYSTEM BEGAN JULY 1973. SEVERAL PROBLEMS THEN DEVELOPED IN THE FORM OF EROSION OF FANS AND THE LIME FEED SYSTEM CAUSING OUTAGES OF THE SCRUBBER SYSTEM. AFTER AND EXTENDED OUTAGE, THE SCRUBBER SYSTEM WAS RETURNED TO SERVICE IN MARCH 1974. THE SYSTEM HAS BEEN OPERATING CONTINUOUSLY SINCE IT RETURNED TO SERVICE WITH VARIOUS NUMBERS OF BOILERS CONNECTED TO THE SCRUBBER SYSTEM AND SCRUBBER TRAINS IN SERVICE.

4/74	SYSTEM	720
5/74	SYSTEM	744
6/74	SYSTEM	720

DUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

7/74 SYSTEM

744

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM CONSISTS OF 1 TWO-STAGE AND 3 ONE-STAGE VENTURI SCRUBBERS. PRESENTLY ONLY THE TWO-STAGE AND 1 ONE-STAGE TRAIN ARE IN SERVICE TREATING FLUE GAS FROM BOILERS 2, 3,AND 4 (ABOUT 40% OF THE STATION CAPACITY). CHRONIC PROBLEMS INCLUDE PUMP EROSION AND FAN VIBRATION.

8/74 SYSTEM

744

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM EXPERIENCED PLUGGING PROBLEMS IN EARLY AUGUST. THE UTILITY IS CURRENTLY INVOLVED IN A RECYCLE PUMP STUDY. CONSIDERATIONS FOR PUMP DESIGN AND MATERIALS ARE BEING MADE TO IMPROVE PUMP LIVE.

9/74 SYSTEM 72

10/74 SYSTEM 744

11/74 SYSTEM 720

## ** PROBLEMS/SOLUTIONS/COMMENTS

SINCE STARTUP IN SEPTEMBER 1973 THE FGD SYSTEM HAS OPERATED AT REDUCED CAPACITY WITH ONLY 2 OR 3 OF THE 4 TRAINS OPERATING AT ANY TIME TREATING FLUE GAS FROM 4 BOILERS (ABOUT 40% OF THE STATION CAPACITY). THE TIE IN OF BOILER NO. 5 DURING NOVEMBER HAS BOOSTED THE FGD SYSTEMS LOAD TO ABOUT 62% OF THE STATION CAPACITY. OVERALL SO2 REMOVAL EFFICIENCY IS 60%. THE TWO-STAGE TRAIN ITSELF REMOVES 80% OF THE INLET SO2. TESTS WITH MAGNESIUM PROMOTED LIME INDICATE THAT SO2 REMOVAL EFFICIENCY CAN BE BOOSTED BY 60% OVER COMMERCIAL LIME.

DURING THE PERIOD REBRACING OF FAN BLADES WAS IN PROGRESS.

12/74 SYSTEM

744

# ** PROBLEMS/SOLUTIONS/COMMENTS

DURING DECEMBER REPAIRS WERE MADE TO HOLES IN THE MIST ELIMINATORS WITH CEILCOTE APPLICATIONS.

FOUR TONS OF SLUDGE WERE REMOVED FROM ONE SCRUBBER BASE. THE VENTURI DAMPERS WERE SEIZING AS A RESULT OF SOLIDS BUILDUP.

THE UTILITY IS AWAITING THE DELIVERY OF SPARE RECYCLE PUMPS.

1/75 SYSTEM

744

## ** PROBLEMS/SOLUTIONS/COMMENTS

THREE SCRUBBING TRAINS OPERATED ON TWO THIRDS OF THE BOILER FLUE GAS OUTPUT. THE SCRUBBING SYSTEM OPERATED ON FLUE GAS FROM FIVE BOILERS THROUGHOUT JANUARY WITH NEARLY 100% FGD SYSTEM AVAILABILITY. OVERALL SO2 REMOVAL EFFICIENCY WAS APPROXIMATELY 60%.

BECAUSE OF SOLIDS BUILDUP THE DAMPERS WERE SEIZING. THE UTILITY HAS BEEN EXERCISING THE DAMPERS MORE FREQUENTLY AS A RESULT AND THIS SEEMS TO HAVE IMPROVED DAMPER OPERATIONS.

DUE TO COLD WINTER WEATHER AND RELATED CONDITIONS THE SLUDGE STABILIZATION PROCESS REQUIRES A LONGER PERIOD OF TIME. THE SLUDGE PONDS HAVE BEEN

DURIUSNE LIGHT: PHILLIPS 1-6 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

FILLING IN 8 TO 9 DAYS. 6 TO 7 DAYS ARE REQUIRED TO EMPTY PONDS. THE CURRENT SLUDGE PRODUCT HAS BEEN A SOUPY CONSISTENCY REQUIRING A CLAMSHELL TYPE DREDGE FOR THE POND. PLUGGING IN THE STABILIZING AGENT INJECTION LINES IS THOUGHT TO HAVE CONTRIBUTED TO THE POOR SLUDGE QUALITY.

SOME WET SIDE SO2 MONITORS FAILED DURING THE PERIOD. THEY ARE CURRENTLY BEING MODIFIED BY THE MANUFACTURER.

THE REHEATERS HAVE NOT YET BEEN TESTED.

2/75 SYSTEM

672

3/75 SYSTEM

744

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE FOURTH FGD TRAIN AND THE SIXTH BOILER WERE TIED IN ON MARCH 17, 1975. ONE OF THE BOILERS WAS DOWN FOR MAINTENANCE SO THE SCRUBBING SYSTEM DID NOT OPERATE ON FLUE GAS FROM ALL SIX BOILERS.

DURING MARCH THE PROGRAM TO IMPROVE SCRUBBER RECYCLE PUMP PERFORMANCE CONTINUED. FOUR OUT OF SIX NEW PUMPS HAVE BEEN INSTALLED.

THE CALCILOX INJECTION SYSTEM LINES HAVE BEEN PLUGGING FREQUENTLY. THE UTILITY IS CONSIDERING A NEW PNEUMATIC DELIVERY SYSTEM FOR CALCILOX.

THE UTILITY IS CURRENTLY LOOKING FOR NEW SLUDGE DISPOSAL SITES.

4/75 SYSTEM

720

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE PRESSURE DROP INSTRUMENTATION AT THE VENTURIS HAS BEEN A PROBLEM AREA.

THE DAMPERS HAVE STILL BEEN SEIZING BECAUSE OF SOLIDS BUILDUP.

ALL SIX BOILERS AND FOUR SCRUBBING TRAINS OPERATED IN AN INTEGRATED MODE IN APRIL. SOME SOLIDS BUILDUP HAS BEEN DISCOVERED AGAIN IN THE SCRUBBING TRAINS.

BECAUSE OF EROSION AND PLUGGING PROBLEMS, A CONTINUOUS WASH IS NOW PERFORMED ON THE MIST ELIMINATORS.

5/75 SYSTEM

744

## ** PROBLEMS/SOLUTIONS/COMMENTS

PRELIMINARY PARTICULATE MATTER REMOVAL EFFICIENCY TESTS SHOWED THAT THE UNIT MEETS THE 0.8 LB/MM BTU ALLEGHENY COUNTY STANDARD. THE OUTLET LOADINGS IN MAY WERE IN THE 0.04 LB/MM BTU RANGE.

A HOLE WAS DISCOVERED IN A SCRUBBER LINER DURING MAY. A PREVIOUSLY PATCHED AREA HAD FAILED AGAIN.

6/75 SYSTEM

720

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM OPERATED ON FLUE GAS FROM ALL SIX BOILERS DURING JUNE. THE TWO-STAGE SCRUBBING TRAIN HAS BEEN OUT OF SERVICE FOR GENERAL MAINTENANCE AND A LINER LEAK REPAIR IN THE FIRST-STAGE SCRUBBER SINCE JUNE 19.

SOME RECYCLE PUMP REPLACEMENTS WERE REQUIRED DURING JUNE.

DUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)

PERFORMANCE DATA								
PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION	% REMOVAL	PER	BOILER	FGD	CAP.			
PERIOD HODOLE AVAILABLE OF COMMENT OF COMMEN	SO2 PART.							
	JOE FARIA	110010	110070	110063	IACIUN			

THE SLUDGE STABILIZATION FACILITY HAS BEEN EXPERIENCING PROBLEMS.

UNBURNED CARBON FINES ARE CAUSING PLUGGING IN THE SCRUBBING SYSTEMS. THE UTILITY HAS BEEN TRYING A WETTING AGENT TO MINIMIZE THE PROBLEM.

PROBLEMS WERE EXPERIENCED WITH THE LIME HANDLING SYSTEM DURING JUNE.

7/75	101	79.1	53.8			
	201	35.5	24.2			
	301	100.0	71.4			
	401	100.0	97.2			
	SYSTEM	90.5	61.6	744	506	458

## ** PROBLEMS/SOLUTIONS/COMMENTS

GENERAL MECHANICAL PROBLEMS WERE EXPERIENCED IN JULY.

8/75	101	97.7	64.2			
	201	100.0	91.7			
	301	66.0	43.4			
	401	65.3	42.9			
	SYSTEM	82.3	60.5	744	489	453

#### ** PROBLEMS/SOLUTIONS/COMMENTS

SCRUBBER UNAVAILABILITY FORCED BOILER NO.6 TO BE RETURNED TO THE SCRUBBER BYPASS PATH IN ORDER TO PREVENT LOSS OF BOILER CAPACITY.

PLUGGING AND MAINTENANCE PROBLEMS HAVE BEEN ENCOUNTERED.

EVALUATION OF VARIOUS RECYCLE PUMPS CONTINUED IN AUGUST.

9/75	101	8.5	7. <b>9</b>			
	201	83.5	77.9			
	301	100.0	95.1			
	401	79.8	74.4			
	SYSTEM	68.0	63.8	720	672	460
10/75	101	88.4	81.6			
	201	30.1	27.8			
	301	73.5	67.9			
	401	70.9	65.5			
	SYSTEM	65.7	60.7	744	687	451

# ** PROBLEMS/SOLUTIONS/COMMENTS

IN OCTOBER 1975, THIOSORBIC LIME SCRUBBING WAS INITIATED IN THE PHILLIPS SINGLE-STAGE SCRUBBING TRAINS ON AN EXPERIMENTAL BASIS. THE UTILITY IS STUDYING COMPLIANCE FEASIBILITY, SOZ REMOVAL EFFICIENCY, AND QUALITY OF THE SLUDGE GENERATED BY THE SINGLE-STAGE SCRUBBING TRAINS.

PRESENTLY ONLY 4 OF THE 6 BOILERS ARE TIED INTO THE FGD SYSTEM.

11/75	101	86.9	86.9			
	201	100.0	100.0			
	301	.0	.0			
	401	10.4	10.4			
	SYSTEM	49.3	49.3	720	720	355
12/75	101	50.8	48.4			
	201	93.2	88.8			
	301	25.7	24.5			
	401	54.4	51.9			
	SYSTEM	56.0	53.4	744	709	397

DUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY CONCLUDED THE THIOSORBIC LIME TESTING PROGRAM IN MID-DECEMBER. FOUR BOILERS WERE COUPLED TO THE SCRUBBING SYSTEM DURING THE RUN. THE UTILITY IS NOW ANALYZING THE DATA GENERATED DURING THE TEST PROGRAM. THE SCRUBBERS HAVE BEEN PUT BACK ON REGULAR LIME. NO UNUSUAL PROBLEMS WERE ENCOUNTERED DURING THE TEST RUN. THE UTILITY HAS STARTED CONSTRUCTION ON AN ADDITIONAL LIME SLAKER FOR FULL SCALE MAGNESIUM PROMOTED LIME OPERATION. THE THICKENER MAY REQUIRE REDESIGN TO ACCOMODATE INCREASED CAPACITY.

1/76	101	38.4	37.2			
	201	74.2	72.0			
	301	14.0	13.6			
	401	97.9	95.0			
	SYSTEM	56.1	54.4	744	722	405

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE 2.5-MONTH TEST PROGRAM WITH THIOSORBIC LIME INCLUDED 1612 HOURS ON ONE TRAIN AND 1309 HOURS ON ANOTHER TRAIN. RESULTS INDICATE THAT THE REQUIRED DEGREE OF S02 REMOVAL (83%) CAN BE OBTAINED WITH AN MGO CONTENT OF 8-10% IN THE LIME WITH SINGLE-STAGE SCRUBBING.

2/76	101	97.8	94.4			
	201	98.5	95.1			
	301	24.7	23.9			•
	401	60.4	58.3			
	SYSTEM	70.4	67.9	6 <del>9</del> 6	672	472
3/76	101		93.4			
	201		47.5			
	301		88.6			
	401		62.0			
	SYSTEM		72.9	744		542
4/76	SYSTEM			720		

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY IS STILL EXPERIENCING PROBLEMS WITH SOLIDS DEPOSITION IN THE VENTURI THROAT OF THE SCRUBBING TRAINS, CAUSING MOVEMENT INHIBITION AND GREATER PRESSURE DROPS.

THE SLUDGE STABILIZATION PRACTICES ARE STILL CONTINUING AT THIS FACILITY.

PLANT OPERATION IS PROCEEDING WITH A TOTAL OF FOUR BOILERS COUPLED INTO THE SCRUBBING SYSTEM (EQUALING 336 MW, WHICH IS 87% OF THE TOTAL PLANT CAPACITY). THE FGD SYSTEM OPERATED ON HIGH CALCIUM LIME DURING THE REPORT PERIOD. THE GENERAL OPERATION MODE AT THIS FACILITY HAS ONE OF THE FOUR SCRUBBING TRAINS OUT CONTINUALLY FOR REPAIRS, CLEANING, AND PREVENTIVE MAINTENANCE. THE FGD SYSTEM AVAILABILITY FOR THE FIRST QUARTER OF 1976 WAS 72%.

5/76 SYSTEM 744 6/76 SYSTEM 720

# ** PROBLEMS/SOLUTIONS/COMMENTS

REDUCED LOAD OPERATIONS WERE REPORTED BY THE UTILITY FOR THE MAY-JUNE PERIOD BECAUSE OF A SCHEDULED TURBINE OVERHAUL ON BOILER NO. 6.

DUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)

-----PERFORMANCE DATA---------------PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS FACTOR 

THE UTILITY IS PROCEEDING WITH THE INSTALLATION OF THREE ADDITIONAL LIME STORAGE SILOS AND A THIRD THICKENER.

THE SCRUBBING SYSTEM WAS SHUT DOWN ON JUNE 27 FOR A SCHEDULED FOUR WEEK REPAIR PERIOD. THE MAJORITY OF THE WORK WILL BE CONCENTRATED ON THE STACK ASSOCIATED DUCTWORK AND BOILER DAMPERS. THE ACID BRICK FLUE HAS BEEN LEAKING PARTICULARLY IN THE MORTAR JOINTS AND STEEL BANDS SUPPORTING THE BRICK HAVE BEEN CORRODING. CORROSION HAS OCCURRED IN THE DUCTWORK IN THE EXPANSION JOINT AREA WHERE THE DUCT ENTERS THE STACK.

THE SLUDGE IS CURRENTLY BEING STABILIZED WITH A CALCILOX ADDITION AT A RATE OF APPROXIMATELY 10% BY WEIGHT OF SLUDGE. THE UTILITY IS PLANNING TO CONTRACT IUCS FOR SLUDGE STABILIZATION IN APPROXIMATELY A YEAR.

7/76 SYSTEM

744

8/76 SYSTEM

744

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE FOUR-WEEK SYSTEM OVERHAUL WAS COMPLETED JULY 25. THE THREE ADDITIONAL LIME STORAGE SILOS AND THE FOUNDATION FOR THE ADDITIONAL 75-FOOT DIAMETER THICKENER HAVE BEEN INSTALLED. WHEN THE NEW EQUIPMENT IS INSTALLED THE UTILITY WILL SWITCH FROM LIME TO MAGNESIUM PROMOTED (THIOSORBIC) LIME. THE UTILITY HAS SIGNED A LETTER OF INTENT WITH IUCS FOR A LONG-TERM SLUDGE TREATMENT SYSTEM.

REPAIRS WERE MADE ON THE TURNING VANES TO THE SCRUBBER MIST ELIMINATORS. THE CEILCOTE COATING ON MODULE 401 FAILED (ORIGINAL COAT ERODDED AWAY AND CORROSION HAD SET IN).

REPAIR WORK WAS COMPLETED ON THE EXPANSION JOINT SEAL WHERE THE DUCTWORK TIES INTO THE MAIN STACK.

THE STEEL BANDS AROUND THE INNER STACK STRUCTURE WERE REPAIRED.

THE SCRUBBERS ID FANS WERE OVERHAULED.

THE BOILER EXIT DAMPERS WERE REPAIRED.

REPAIRS WERE MADE TO STOP LEAKING IN THE ACID-BRICK FLUE OF THE MAIN STACK.

9/76 SYSTEM

720

10/76 SYSTEM

744

## ** PROBLEMS/SOLUTIONS/COMMENTS

BOILER NUMBERS 2 THROUGH 6 WERE COUPLED INTO THE SCRUEBING SYSTEM. BOILER NO. 1 IS DOWN FOR OVERHAUL AND REPAIRS. THE IUCS INTERIM SLUDGE PROCESS-ING PLANT IS UNDER CONSTRUCTION AND WILL BE IN SERVICE BY DECEMBER 1976. THE TEMPORARY FACILITIES WILL PROCESS THE THICKENER UNDERFLOW AND PONDED SLUDGE UNTIL THE POND IS DEPLETED OF SLUDGE AND THE PERMANENT FACILITY HAS BEEN INSTALLED. SCRUBBING OPERATIONS ARE STILL PROCEEDING IN AN OPEN WA-TER LOOP MODE WITH PART OF THE THICKENER OVERFLOW BEING DIVERTED TO THE ASH POND. BECAUSE BOTH THE BEAVER VALLEY AND BRUCE MANSFIELD STATIONS ARE FULLY OPERATIONAL, THIS STATION HAS BEEN RELEGATED TO PEAK LOAD OPERA-TIONS. GENERAL LOAD OPERATIONS ARE FULL LOAD CAPACITY IN THE DAYTIME AND 50 TO 67% LOAD REDUCTION AT NIGHT.

TOTAL SCRUBBER HOURS: 23,274 TOTAL BOILER HOURS: 83,642 TOTAL SCRUBBER AVAILABLE

THE FIGURES AT THE LEFT WERE COMPILED BY THE UTILITY FOR SYSTEM OPERATIONS TOTAL SCRUBBER OUTAGE TIME: 5,500 FOR THE PERIOD FOLLOWING START-UP IN JULY 1973 INCLUSIVE TO OCTOBER 1976.

NUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)

_____PERFORMANCE DATA______ PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR _____

HOURS: 23,274 THE TOTAL SCRUBBER HOURS VALUE IN-AVERAGE MW LOAD/SCRUBBER OPERATION CLUDES OPERATION TIME WHEN ONE OR

HOUR: 243

TOTAL OPERABILITY INDEX: 28% TOTAL RELIABILITY INDEX: 81% MORE OF THE MODULES WERE IN SERVICE. TOTAL BOILER AND UNAVAILABILITY VAL-UES APPLY FOR ALL THE CORRESPONDING UNITS. THE TOTAL SCRUBBER AVAILABIL-TY INDEX INCLUDES THE TIME WHEN ONE

OR MORE MODULES WERE AVAILABLE FOR SERVICE.

11/76 SYSTEM

720

12/76 SYSTEM

744

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE IUCS SLUDGE STABILIZATION FACILITY AT PHILLIPS WAS INSTALLED AND STARTED UP IN DECEMBER. THE FACILITY INCLUDES EQUIPMENT FOR DEWATERING, ESP-COLLECTED FLYASH ADDITION AND TRANSPORT TO THE OFF-SITE LANDFILL.

THE RECYCLE PUMP EVALUATION IS CONTINUING. AFTER 2500 HOURS OF OPERATION THE PUMPS USING CARBORUNDUM WEAR RINGS AND CD4 MCU IMPELLERS WERE HOLDING UP WELL. THEY HAVE NOW ACCUMULATED 2800 HOURS OF OPERATION (THEY WERE INSPECTED AFTER 2500 HOURS). AFTER 2900 HOURS OF OPERATION PUMPS USING CARBORUNDUM WEAR RINGS AND TITANIUM IMPELLERS WERE PERFORMING WELL.

BOILERS 2 THROUGH 6 WERE COUPLED INTO THE SYSTEM THROUGHOUT THE PERIOD. BOILER 1 REMAINED SHUT DOWN.

THE FIRST NEW SLAKER (PASTE TYPE SLAKER), ONE OF FOUR NEW UNITS CAME ON LINE DURING THE PERIOD. HIGHER STOICHIOMETRIC RATIOS, HIGHER PH VALUES AND INCREASED SO2 REMOVAL EFFICIENCY RESULTED IN THE SYSTEMS.

IN ORDER TO ENHANCE SETTLING IN THE TWO 75-FOOT DIAMETER THICKENERS A POLYELECTROLYTE MATERIAL WILL BE ADDED ON A TEMPORARY BASIS. WHEN THE NEW 75-FOOT THICKENER IS BROUGHT ON LINE THE POLYELECTROLYTE ADDITION IS EXPECTED TO BE TERMINATED.

THE CONTRACT WITH DRAVO FOR THIOSORBIC LIME (MG-PROMOTED LIME) HAS BEEN FINALIZED. THE SWITCH TO MAGNESIUM PROMOTED LIME WILL TAKE PLACE WHEN THE LAST THICKENER IS COUPLED INTO THE SYSTEM.

THE VENTURIS ARE ENCOUNTERING A GREAT DEAL OF SCALING. PRESSURE DROPS ACROSS THE VENTURIS ARE REGISTERING TWICE THE NORMAL PRESSURE DROP AT 12 INCHES H2O(6 INCHES H2O IS DESIGN).

1/77 SYSTEM

744

2/77 SYSTEM

672

## ** PROBLEMS/SOLUTIONS/COMMENTS

1977 FULL COMPLIANCE OPERATIONS WILL INCLUDE 83% S02 REMOVAL FOR 2% SULFUR COAL UTILIZING THIOSORBIC LIME (6-12% MG) AND FIXATING THE SCRUBBER WASTES WITH THE IUCS POZ-O-TEC METHOD. THE FIXATED MATTER WILL BE HAULED AWAY TO AN OFF-SITE DISPOSAL AND LANDFILL. IUCS HAS BEEN AWARDED A TEN YEAR CON-TRACT FOR THE USE OF THIS METHOD.

3/77 SYSTEM

744

4/77 SYSTEM

720

DUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART, HOURS HOURS FACTOR

## ** PROBLEMS/SOLUTIONS/COMMENTS

ALL SIX BOILERS ARE COUPLED INTO THE FGD SYSTEM.

THE RECYCLE PUMP EVALUATION IS CONTINUING. THE CARBORUNDUM IMPELLERS AND WEAR RINGS ARE PERFORMING WELL AFTER 4000 OPERATING HOURS.

CONSTRUCTION OF THE THICKENERS AND LIME FEEDERS IS STILL CONTINUING. FULL PLANT COMPLIANCE SHOULD OCCUR BY DECEMBER 1977 WHEN THE NEW THICKENERS AND SLAKERS COME ON LINE.

THE IUCS FACILITY IS JUST FILTERING OUT WATER. NO FIXATIVE IS BEING ADDED. THE WASTE ARE BEING HAULED AWAY TO AN OFF-SITE LANDFILL ONE MILE FROM THE STATION.

SO2 AND PARTICULATE MATTER REMOVAL EFFICIENCIES ARE 50 AND 99+% RESPECTIVELY.

1975 THIOSORBIC LIME TESTS SHOWS THAT 8% MGO IN THE LIME WAS OPTIMUM FOR SO2 REMOVAL BUT IT IS POSSIBLE TO GO AS HIGH AS 12% MGO. LIME ARRIVING AT PHILLIPS WILL HAVE A 6% MGO CONCENTRATION. IT WILL BE POSSIBLE TO BLEND THE LIME TO ACHIEVE HIGHER MGO AT THE STATION IF NECESSARY.

# 5/77 SYSTEM 720

## ** PROBLEMS/SOLUTIONS/COMMENTS

DAMPER AND MIST ELIMINATOR REPAIRS WILL BE CORRECTED DURING THE NEXT SCHEDULED OUTAGE. OVERALL SCRUBBER OPERABILITY IS ABOUT 75%.

THIOSORBIC LIME TESTS BEGAN IN LATE MAY BUT LASTED ONLY ABOUT ONE WEEK.

THE SCRUBBER SYSTEM WAS SHUT DOWN FOR THREE TO FOUR DAYS IN MAY DUE TO LEAKING IN THE WET DUCT HEADER THAT LEADS TO THE STACK. WHEN THE LEAK WAS REPAIRED SCRUBBING OPERATIONS BEGAN AGAIN ON FLUE GAS FROM FOUR BOILERS.

WHILE FIXING A DUCT LEAK INSPECTION OF OTHER COMPONENTS REVEALED THAT THE BOILER EXIT DAMPERS WERE ERODING.

ONE OF THE MODULE 201 EXTERNAL MIST ELIMINATORS WAS SEVERLY ERODED AND PLUGGED.

THE INTERIM SLUDGE DISPOSAL SYSTEM IS STILL OPERATIONAL. THE PERMANENT SLUDGE DISPOSAL FACILITY IS ON SCHEDULE FOR THE DECEMBER 1977 COMPLETION DATE.

THE CARBORUNDUM WEAR RINGS AND IMPELLERS WERE CONTINUING TO PERFORM WELL AFTER 5000 OPERATING HOURS.

6/77 SYSTEM

720

7/77 SYSTEM

744

# ** PROBLEMS/SOLUTIONS/COMMENTS

ALL SIX BOILERS ARE COUPLED INTO THE SCRUBBER PLANT. FLUE GAS FROM FIVE OF THESE UNITS IS BEING TREATED BY THE SCRUBBERS. ONLY FOUR OF THE SIX BOILERS ARE ACTUALLY OPERATING BECAUSE OF THE CURRENT TURBINS REPAIR OUTAGE. OPERATIONS ARE PROCEEDING WITH ONE SCRUBBING TRAIN OUT OF SERVICE AT ALL TIMES FOR MAINTENANCE AND CLEANOUT. SO2 REMOVAL EFFICIENCY IS APPROXIMATELY 50%.

NUGUESNE LIGHT: PHILLIPS 1-6 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

BOILER 6 HAS BEEN OUT OF SERVICE WHILE TURBINE REPAIRS ARE BEING MADE.

THE RECYCLE PUMP EVALUATION STUDY CONTINUED DURING THE PERIOD. COMPONENTS BEING EVALUATED INCLUDE: CARBORUNDUM IMPELLERS, CARBORUNDUM WEAR RINGS, TITANIUM IMPELLERS, 317SS WEAR RINGS AND STELLITE TIPPED IMPELLERS.

A THIOSORBIC LIME TEST WAS PREMATURELY TERMINATED BECAUSE OF SOME MINOR SLAKER/FEEDER PROBLEMS. HIGH CALCIUM VIRGIN LIME WAS UTILIZED DURING THE MAJORITY OF OPERATIONS THROUGHOUT THE PERIOD.

8/77 SYSTEM 744 9/77 SYSTEM 720

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## ** PROBLEMS/SOLUTIONS/COMMENTS

LIME HANDLING AND SOLID WASTE DISPOSAL FACILITIES WERE BEING SCALED UP TO HANDLE FULL CAPACITY AND A THIRD THICKENER WAS INSTALLED AND BROUGHT INTO SERVICE DURING THIS REPORT PERIOD. THE IUCS SYSTEM IS STILL PERFORMING INTERIM PHASE OPERATIONS. WASTE WATER IS BEING MIXED WITH FLYASH AND DISPOSED WITHOUT FIXATIVE ADDITION. CURRENT CONSTRUCTION WORK IS EXPECTED TO BE COMPLETED BY THE END OF JANUARY WHEN ALL SIX BOILERS WILL BE BACK ON LINE FOR A TWO MONTH TEST PERIOD. THIOSORBIC LIME IS STILL BEING TESTED. RESULTS ARE NOT YET AVAILABLE. THE FGD SYSTEM WILL BE DOWN FOR THE FIRST WEEKEND OF NOVEMBER. THE SYSTEM WILL ALSO BE CHECKED FOR MAIN DUCT LEAKS AT THIS TIME. THE SCRUBBER AND STACK LININGS AND RECYCLE PUMPS WILL BE THOROUGHLY CHECKED AS WELL. NECESSARY REPLACEMENTS AND REPAIRS WILL BE CARRIED OUT. CURRENT SO2 REMOVAL EFFICIENCY IS 50%. BY EARLY APRIL 1978 THE SYSTEM IS EXPECTED TO REACH COMPLIANCE WITH AN SO2 REMOVAL EFFICIENCY OF 83%.

10/77	101	92.6	92.6
	201	4.0	4.0
	301	88.3	88.3
	401	87.7	87.7
	SYSTEM		

744 744 507

# ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE 101 WAS DOWN A TOTAL OF 113 HOURS IN OCTOBER FOR REGULAR MAINTEN-_ ANCE AND REPAIRS.

MODULE 201 WAS PUT IN SERVICE ON OCTOBER 26 AFTER EXTENSIVE CLEAN UP. ALSO REPAIRS TO THE ID FAN HOUSING RUBBER LINING WERE MADE AND THE FAN WAS BALANCED.

MODULE 301 WAS DOWN A TOTAL OF 57 HOURS IN OCTOBER FOR MAINTENANCE AND REPAIRS.

MODULE 401 WAS DOWN A TOTAL OF 36 HOURS IN OCTOBER FOR REPAIR OF HOLES IN THE ID FAN LINING AND FOR THE TIE-IN OF THE THICKENER BLEED LINE.

11/77	101	92.1	92.1			
	201	91.6	91.6			
	301	28.1	28.1			
	401	56.3	56.3			
	SYSTEM	67.0	67-0	720	720	483

## ** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE SHUTDOWN OUTLET DUCT LEAKS WERE REPAIRED.

BOILER EXIT DAMPERS WERE REPLACED. THE OLD DAMPERS FAILED DUE TO FLYASH EROSION.

DUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

CORROSION OF STEEL BANDS IN STACK WAS DISCOVERED DURING THE PERIOD. THE CORROSION IS A RESULT OF CONDENSED MOISTURE SEEPING THROUGH THE MORTAR.

SLUDGE HANDLING PROBLEMS HAVE OCCURRED BECAUSE DEWATERING OPERATIONS ARE NOT WORKING PROPERLY.

THE RESULTS FROM THIOSORBIC LIME USE CAN NOT YET BE QUANTIFIED DUE TO LIME FEED SYSTEM PROBLEMS.

LIME FEED SYSTEM PROBLEMS OCCURRED OVER THE PERIOD.

THE MIST ELIMINATORS WERE CLEANED DURING NOVEMBER.

12/77	SYSTEM			744		
1/78	101	84.3	84.3			
	201	77.2	77.2			
	301	. 0	.0			
	401	65.1	65.1			
	SYSTEM	56.6	56.7	744	744	421

#### ** PROBLEMS/SOLUTIONS/COMMENTS

CUMULATIVE HOURS FOR JANUARY 1, 1977 THROUGH JANUARY 8, 1978 WERE 22391 FOR MODULE 101, 20998 FOR MODULE 201, 22229 FOR MODULE 301 AND 22259 FOR MODULE 401.

SCRUBBER TRAIN 301 WAS DOWN FOR AN OVERHAUL FROM NOVEMBER 17 TO FEBRUARY 6, 1978 WHEN IT WAS RETURNED TO SERVICE.

SCRUBBER TRAIN 401 WAS REMOVED FROM SERVICE ON FEBRUARY 6.

THE IUCS INTERIM SLUDGE TREATMENT SYSTEM HAS SOME DEWATERING PROBLEMS. DURING DECEMBER PHILLIPS EXPERIENCED POOR SLUDGE REMOVAL. THE IUCS PLANT IS WORKING ON A PART TIME BASIS. FULL OPERATIONS ARE EXPECTED LATE THIS SPRING. THE POOR QUALITY SLUDGE IS SENT TO AN EMERGENCY POND AND THEN RECIRCULATED BACK TO THE THICKENER.

TESTING WITH THIOSORBIC LIME AT 5% MGO HAS SHOWN THAT THE MGO CONCENTRATION IS NOT GREAT ENOUGH TO EFFECT ADEQUATE SO2 REMOVAL ON A SINGLE STAGE SCRUBBER. THE UTILITY IS GOING TO TEST AT A GREATER MGO CONCENTRATION BY STARTING AT 10% AND THEN DROPPING BACK UNTIL THE CONCENTRATION IS SATISFACTORY. THIS TESTING, AS WELL AS SCRUBBER OPERATIONS, HAVE, HOWEVER, BEEN HAMPERED BY LOW LOADS AS A RESULT OF THE COAL STRIKE.

AN OUTAGE HAS BEEN SCHEDULED AT PHILLIPS TO REPLACE THE CARBON STEEL SUPPORT BANDS IN THE STACK WITH STAINLESS STEEL BANDS.

2/78	101		43.5	31.1			
	201		58.5	41.8			
	301		3.8	2.7			
	401		31.7	22.6			
	SYSTEM		34.4	24.6	672	480	167
3/78	SYSTEM	.0		.0	744	0	0

# ** PROBLEMS/SOLUTIONS/COMMENTS

AN OUTAGE OCCURRED BETWEEN JANUARY 6 AND JANUARY 8 WHEN THE STACK DRAIN LEAKS WERE REPAIRED BY SANDBLASTING THE OUTER WALL AND REPLACING THE CARBON STEEL BANDS WITH STAINLESS STEEL BANDS.

THE SYSTEM WAS SHUTDOWN ON FEBRUARY 11 DUE TO THE COAL SHORTAGE. THE OUTAGE CONTINUED THROUGH MARCH AND THE SYSTEM IS SCHEDULED TO BE ON LINE BY

DUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

APRIL 15. DURING THE OUTAGE A NUMBER OF REPAIRS AND MODIFICATIONS WERE MADE.

THE BOILER EXIT DAMPERS WERE LINED WITH 316 SS ON AREAS OF HIGH EROSION CAUSED BY FLYASH IMPINGEMENT.

EXPANSION JOINTS ON THE INLET DUCTWORK WERE SHIELED BY METAL PLATES WHICH WERE WELDED AT ONE END.

NUMEROUS HOLES IN THE WET GAS DUCT WORK WERE REPAIRED AND THE DUCTS WERE RELINED WITH CEILCOTE.

THE VENTURI THROAT DAMPERS WERE CLEANED ON ALL THE SCRUBBERS.

INTERNAL MIST ELIMINATORS WERE CLEANED. THE EXTERNAL MIST ELIMINATORS, WHICH ARE BADLY DETERIORATED, MAY BE REPLACED.

THE STACK ACID BRICK FLUE WAS INSPECTED AND SOME BRICKS WERE REPLACED AT THE TOP OF THE STACK.

CONSTRUCTION WORK ON ADDITIONAL EQUIPMENT SUCH AS THE THICKENER AND SILOS IS ALMOST COMPLETE. IT WAS NOTED THAT THE CEILCOTE LINER COROLINE 505AR HAS HELD UP WELL OVER THREE YEARS ON THE CONICAL APEX OF MODULE 401.

 4/78
 SYSTEM
 720
 528

 5/78
 SYSTEM
 744
 744

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM CAME BACK ON LINE AFTER THE COAL STRIKE IN LATE MARCH. IT IS NOT OPERATING AT FULL LOAD BECAUSE THE NO. 6 BOILER IS STILL OUT AND SHOULD BE BACK ON LINE IN MID-JULY. COMPLIANCE TESTS WILL TAKE PLACE IN JULY, AFTER BOILER 6 IS BACK ON LINE, TO SEE IF THE SYSTEM IS MEETING THE 83% SO2 REMOVAL REQUIREMENT FOR 2% SULFUR COAL. THERE WERE NO HOURS REPORTED FOR THIS PERIOD BECAUSE OF PRELIMINARY TESTING BEING CONDUCTING IN PREPARATION FOR THE COMPLIANCE TESTS. SO FAR, TESTS INDICATE THAT THE SYSTEM WILL COMPLY WITH THE REQUIRED STANDARDS. THE OPERABILITY FOR ALL FOUR TRAINS WAS BETWEEN 65 AND 75%.

6/78	SYSTEM				720	72 <b>0</b>	
7/78	101	48.3	48.3	48.3			
	201	43.9	43.9	43.9			
	301	85.7	78.7	78.7			
	401	82.5	76.0	76.0 -			
	SYSTEM	65.1	61.7	61.7	744	744	459

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE INTERNAL MIST ELIMINATOR ON MODULE 201 WAS REPLACED AND THE MODULE 301 MIST ELIMINATORS WERE CLEANED OVER THE PERIOD.

THE FGD SYSTEM HAS ACCUMULATED APPROXIMATELY 24000 HOURS OF OPERATION ON ALL FOUR MODULES SINCE START-UP.

WATER BALANCE PROBLEMS HAVE CONTRIBUTED TO THE OCCURRANCE OF LOW PH, RESULTING IN MIST ELIMINATOR PLUGGING.

THE MIST ELIMINATOR PLUGGING IS ALSO RELATED TO LOW PH RESULTING FROM LIME HANDLING AND SLURRY PREPARATION SYSTEM FAILURE.

THE UTILITY IS CURRENTLY STUDYING WAYS TO TIGHTEN THE WATER BALANCE BY USING THICKENER SUPERNATANT INTERMITTENTLY WITH CLEAR SERVICE WATER FOR

DUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

THE MIST ELIMINATORS.

THE LIME HANDLING FACILITY DOES NOT INCLUDE A GRIT REMOVAL STAGE. GRIT IS CAUSING PLUGGING IN THE SLURRY HANDLING SYSTEM AND MIXING EQUIPMENT.

PROCESS CHEMISTRY CONTROL IS A CHRONIC PROBLEM AT PHILLIPS DUE IN PART TO TO WATER BALANCE AND LIME HANDLING EQUIPMENT.

WHEN WATER BALANCE IS ACHIEVED THE FGD SYSTEM EXPERIENCES A BUILD UP OF SALTS.

8/78	101	100.0	97.3	97.3			
	201	73.2	71.9	71.9			
	301	100.0	88.8	88.8			
	401	92.4	85.0	85.0			
	SYSTEM	91.4	85.8	85.8	744	744	638

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE RUBBER LINING IN MODULE 101 WAS REPAIRED.

HIGH PRESSURE WATER CLEANING WAS PERFORMED ON MODULES 101 AND 401.

9/78	101	63.7	62.4	62.4			
	201	82.7	75.6	75.6			
	301	83.9	67.5	67.5			
	401	65.6	55.7	55.7			
	SYSTEM	74.0	65.3	65.3	720	720	470

## ** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE AUGUST-SEPTEMBER PERIOD MIST ELIMINATOR CLEANING TOOK PLACE IN ORDER TO CORRECT THE PLUGGING PROBLEM.

IN AUGUST THE INTERNAL MIST ELIMINATOR ON MODULE 201 WAS REPLACED.

THE LIME MIXING BASIN HAD TO BE SHUT DOWN OVER A WEEKEND SO THAT EXCESSIVE GRIT AND SOLID PARTICLES THAT HAD BUILT UP COULD BE CLEANED OUT.

HIGH PRESSURE WATER CLEANING WAS PERFORMED ON MODULES 101 AND 401.

THE RUBBER LINING IN MODULE 101 WAS REPAIRED.

A MAJOR PROBLEM AREA DURING THE PERIOD WAS CAUSED BY INSUFFICIENT SUPPLIES OF DRY FLYASH TO MIX WITH THE SLUDGE. AS A RESULT THE SLUDGE HAS BEEN LEAKING OUT OF THE TRANSPORT TRUCKS WHILE IN TRANSIT TO THE FINAL DISPOSAL SITE. APPARENTLY NOT ENOUGH FLYASH IS BEING COLLECTED WITH THE PRESENT SYSTEM.

10/78	101	100.0	96.1	96.1			
	201	97.7	87.5	87.5			
	301	95.3	87.9	87.9			
	401	4.8	2.2	2.2			
	SYSTEM	74.5	68.4	68.4	744	744	509
11/78	101	44.0	41.1	41.1			
	201	100.0	100.0	100.0			
	301	91.7	88.9	88.9			
	401	71.3	69.0	69.0			
	SYSTEM	76.8	74.8	74.8	720	720	538

DUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

## ** PROBLEMS/SOLUTIONS/COMMENTS

SO2 AND PARTICULATE MATTER REMOVAL EFFICIENCY TESTS INDICATE THAT THE STATION NOW MEETS STATE STANDARDS.

THE FGD SYSTEM IS EXPERIENCING A LARGE AMOUNT OF SCALING BECAUSE OF THE HIGH EXCESS AIR ENTERING THE SYSTEM FROM THE BOILERS OXIDIZING THE SOFT SULFITE TO SULFATE ON THE SCRUBBER INTERNALS.

12/78	101	91.7	90.8	90.8			
	201	98.0	88.1	88.1			
	301	30.3	27.8	27.8			
	401	90.4	87.5	87.5			
	SYSTEM	77.6	73.6	73.6	744	744	547

## ** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE PERIOD A LACK OF FLYASH FOR MIXING WITH SLUDGE RESULTED IN A WET SLUDGE PRODUCT THAT MUST BE LEFT ON SITE TO DRY BEFORE TRANSPORT TO THE LANDF\ILL.

1/79	101 201 301	89.0 77.9 50.1	86.8 69.2 50.0	86.8 69.2 50.0			
2770	401 SYSTEM	86.1 75.8	83.7 72.4	83.7 72.4	744	744	539
2/79	101 201 301 401 SYSTEM	38.9 72.1 88.3 100.0 74.8	38.9 72.1 88.3 100.0 74.8	38.9 72.1 88.3 100.0 74.8	672	672	503

## ** PROBLEMS/SOLUTIONS/COMMENTS

EXCESSIVE SCALING IN THE MODULE 101 EXIT DUCT CAUSED SUPPORT COLUMNS TO COLLAPSE. THE SCALE WAS REMOVED AND THE SUPPORT COLUMNS WERE SHORED UP.

3/79	101 201 301 401 SYSTEM	.0 96.6 97.6 100.0 73.6	.0 96.3 88.0 100.0 71.1	.0 96.3 88.0 100.0 71.1	744	744	529
4/79	101 201 301 401 SYSTEM	89.9 5.9 97.6 89.0 70.6	86.8 5.9 85.0 84.9 65.7	86.8 5.9 85.0 84.9 65.7	720	720	473
5/79	101 201 301 401 SYSTEM	100.0 .0 99.3 99.4 74.7	100.0 .0 96.6 99.2 74.0	100.0 .0 96.6 99.2 74.0	744	744	550
6/79	101 201 301 401 SYSTEM	70.8 28.8 85.6 85.5 67.7	70.5 22.2 83.7 77.2 63.4	70.5 22.2 83.7 77.2 63.4	720	720	457
7/79	101	100.0	98.6	98.6			

DUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)

				PERFORMA	NCE DATA						
PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% RE	MOVAL PART.	PER HOURS	BOILER HOURS	HOURS	CAP. FACTOR
	201	98.5	95.8		95.8						
		72.7			71.4						
		29.9			25.5						
		75.3			72.8			744	744	542	
8/79	101	100.0	100.0		100.0						
	201	97.6	89.5		89. <b>5</b>						
	301	100.0	89.3		89.3						
	401	.0	.0		.0						
	SYSTEM	74.4	69.7		69.7			744	744	519	
9/79	101	88.8	81.8	88.8	81.8						
	201	94.8	80.3	93.9	80.3						
	301	99.6	85.5	99.6	85. <b>5</b>						
	401	.0	.0	٥.	.0						
	SYSTEM	70.8	61.9	70.4	61.9			720	720	446	
10/79	101	99.4		99.3	97.0						
	201	86.5	86.6	86.6	86.6						
	301	93.8	93.0	93.7	93.0						
	401	.0	.0	.0	. 0						
	SYSTEM	69.9	69.2	69.9	69.2			744	696	515	
11/79	101	53.0	50.7	51.9							
	201	99.0		99.0							
	301	83.6	83.6	83.6	83.6						
	401	11.5	11.5	11.6	11.5						
	SYSTEM	61.8	61.2	61.5	61.2			720	720	441	
12/79	101	.0	. 0	.0	.0						
	201		98.6		98.6						
	301	90.7	89.6	90.6	89.6						
	401	77.7	72.9	76.6							
	SYSTEM	67.1	65.3	66.8	65.3			744	744	486	

^{**} PROBLEMS/SOLUTIONS/COMMENTS

PRESENTLY THE UTILITY HAS BEEN ADDING SODIUM THIOSULFATE TO THE LIME TO PREVENT SCALE FORMATION. THIS PROCESS HAS IMPROVED SO2 COLLECTION AS WELL.

THE SCRUBBER FAN HOUSING LINERS ARE BEING REPLACED.

THE MECHANICAL COLLECTORS ARE BEING UPGRADED TO IMPROVE THE QUALITY OF THE WET SLUDGE.

1/80	101	.0	.0	.0	.0			
	201	98.1	93. <b>3</b>	98.0	93.3			
	301	100.0	99.0	100.0	99. <b>0</b>			
	401	97.6	95.8	97.5	95.8			
	SYSTEM	73.9	72.0	73.9	72.0	744	744	536
2/80	101	13.7	13.7	13.7	13.7			
	201	91.6	91.6	91.7	91.6			
	301	86.2	84.6	86.0	84.6			
	401	94.2	90.5	94.0	90.5			
	SYSTEM	71.4	70.1	71.4	70.1	696	696	488

^{**} PROBLEMS/SOLUTIONS/COMMENTS

SODIUM THIOSULFATE ADDITION CONTINUED THROUGH THE FIRST QUARTER RESULTING IN A INCIDENCE OF SIGNIFICANTLY REDUCED MIST ELIMINATOR SCALING. 2000-5000 HOURS OF OPERATION HAVE BEEN LOGGED WITHOUT MIST ELIMINATOR SCALE ACCUMULATION. THE UTILITY REPORTED THAT SO2 REMOVAL EFFICIENCY HAS

407

DUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAR.

SO2 PART. HOURS HOURS FACTOR

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IMPROVED 3% DUE TO THE SODIUM THIOSULFATE ADDITION. THE UTILITY IS LOOKING INTO SODIUM THIOSULFATE ADDITION AT ELRAMA.

THE FAN RUBBER LINERS HAVE BEEN A CONTINUAL PROBLEM. TWO FANS WILL BE REPLACED WITH INCONEL THE NEXT TIME THE RUBBER LINERS FAIL.

THE PHILLIPS FGD SYSTEM HAD A SYSTEM AVAILABILITY OF 71.8% FOR THE YEAR 1979.

3/80	101	94.7	84.0	94.0	84.0		
	201	59.0	53.9	56.8	53.9		
	301	48.4	40.3	43.8	40.3		
	401	95.4	95.3	99.8	95.3		
	SYSTEM	60.3	54.7	73.6	54.7	744	744

### ** PROBLEMS/SOLUTIONS/COMMENTS

PROBLEMS WERE ENCOUNTERED WITH THE MODULE 101 ID FAN. THE MODULE WAS TAKEN OFF LINE SO THE ID FAN COULD BE BALANCED.

PROBLEMS WERE ENCOUNTERED WITH THE HUB BOLTS ON THE ID FAN OF MODULE 201, CAUSING THE MODULE TO COME OFF LINE FOR 11 DAYS.

THE RUBBER LINING ON THE ID FAN HOUSING OF MODULE 301 NEEDED REPAIR DURING MARCH.

MODULE 401 WAS TAKEN OFF LINE FOR APPROXIMATELY 2 HOURS SO REPAIRS COULD BE MADE ON THE SCRUBBER MAKE-UP VALVES.

4/80	101	92.6	89.4	92.4	89.4			
	201	14.2	10.0	10.5	10.0			
	301	99.2	99.0	99.8	99.0			
	401	95.8	94.6	98.6	94.6			
	SYSTEM	96.9	.73.3	75.6	73.3	720	720	527

### ** PROBLEMS/SOLUTIONS/COMMENTS

ON APRIL 5 MODULE 101 WAS TAKEN OFF LINE DUE TO ID FAN BEARING PROBLEMS. LATER IN THE MONTH THE MODULE WAS SHUTDOWN DUE TO AN ID FAN INSTRUMENTATION PRESSURE SWITCH PROBLEM.

TOWARDS THE LATTER PART OF APRIL, MODULE 201 WAS SHUTDOWN DUE TO ID FAN BEARING PROBLEMS. THIS PROBLEM WAS CORRECTED BY BALANCING THE FAN.

MODULE 301 WAS REMOVED FROM OPERATION ON APRIL 11 DUE TO AN ID FAN MOTOR MALFUNCTION.

THE RECYCLE PUMP PACKING ON MODULE 401 NEEDED TO BE REPLACED DURING THE MONTH.

5/80	101	67.5	53.9	62.3	53.9			
3, 00								
	201	81.6	69.0	78.9	69.0			
	301	91.7	73.1	89.8	73.1			
	401	92.2	75.9	90.6	75.9			
	SYSTEM	83.2	68.0	80.2	68. <b>0</b>	744	744	506

### ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE 101 CAME OFF LINE IN MAY SO REPAIRS COULD BE MADE ON THE CONTROL DAMPER AND TO INSTRUMENTATION.

DURING MAY MODULE 201 EXPERIENCED PROBLEMS WITH THE MIST ELIMINATOR AND THE ID FAN. THE MODULE WAS TAKEN OFF LINE FOR APPROXIMATELY TWO DAYS TO WASH THE MISTELIMINATOR INTERNALS AND ONE DAY TO REPAIR THE ID FAN BEARING.

DUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

MODULE 301 EXPERIENCED ID FAN PROBLEMS AND WAS TAKEN OFF LINE WHILE THE ID FAN WAS BALANCED.

MODULE 401 WAS SHUTDOWN APPROXIMATELY 58 HOURS SO THAT THE ID FAN CONTROL DAMPERS COULD BE INSPECTED.

6/80	101	97.1	86.3	96. <b>5</b>	80.5
	201	100.0	81.7	100.0	76.2
	301	75.5	69.4	72.6	64.8
	401	100.0	76.5	100.0	71.4
	SYSTEM	93.2	78.5	91.5	73.2

** PROBLEMS/SOLUTIONS/COMMENTS

THE MODULE 101 MIST ELIMINATOR WAS CLEANED DURING JUNE.

DURING JUNE MODULE 301 WAS DOWN FOR ID FAN HOUSING REPAIRS (RUBBER LINING) CAUSING APPROXIMATELY 176 HOURS DOWN TIME.

720 672 527 55.3

744

744

648 71.4

614 58.5

318 30.1

744

744

720

720

7/80	101	94.0	86.2	93 <b>.5</b>	86.2
•	201	100.0	94.7	100.0	94.7
	301	94.7	84.1	94.0	84.1
	401	91.1	83.5	90.3	83.5
	SYSTEM	94.9	87.1	94.5	87.1

** PROBLEMS/SOLUTIONS/COMMENTS

DURING JULY THE RECYCLE PUMP IMPELLERS WERE REPLACED ON ALL THE MODULES EXCEPT FOR MODULE 201.

8/80	101	91.1	72.9	90.6	72.9
	201	96.9	85.8	96.5	85.8
	301	87.6	85.3	89.6	85.3
	401	92.3	86.1	91.8	86.1
	SYSTEM	92.0	82.5	91.5	82.5

** PROBLEMS/SOLUTIONS/COMMENTS

DURING AUGUST MODULE 401 EXPERIENCED PACKING PROBLEMS WITH THE RECYCLE

DURING THE PERIOD OF JUNE THROUGH AUGUST THE RUBBER LININGS ON THE FAN HOUSINGS WERE REPAIRED.

9/80	101	55.8	55.8	60.9	55.8
	201	46.1	41.7	43.6	41.7
	301	54.9	46.2	50.6	46.2
	401	60.6	32.9	45.5	32.9
	SYSTEM	54.4	47.3	47.0	44.2

** PROBLEMS/SOLUTIONS/COMMENTS

ON SEPTEMBER 20 THE ENTIRE PLANT WAS SHUTDOWN FOR A SCRUBBER INSPECTION. THE INSPECTION REVEALED THAT THERE IS EXTENSIVE MORTAR DETERIORATION IN THE STACK AND THAT REPAIRS WILL BE NECESSARY WITHIN THE NEXT TWO YEARS.

THE INSPECTION LASTED UNTIL OCTOBER 1 DUE TO THE NECESSARY REPAIR OF A DUCT EXPANSION JOINT AND THE REPAIR OF THE UPPER PORTION OF THE STACK JOINTS.

10/80	101	94.2	94.2	94.2	94.2
	201	93.9	90.1	93.5	90.1
	301	4.0	4.0	4.0	4.0

DUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)

			Y OPERABILITY		Y UTILIZATION	<b>S</b> 02	PART.	HOURS	HOURS	HOURS	FACTOR
			92.6	93.6	92.6						
	SYSTEM	71.5	70.2		70.2			744	720	523	58.2
	** PROBLE	EMS/SOLUTI	CONS/COMMENTS								
			DURING OCTOBER		MODULES 301 A	ND 401	WERE	RELINEC	HTIW	CEILCO	ΓE
	101	F3 F	50.8	<b>51.0</b>	50.0						
1/80	101 201	100.0			50.8						
	301	95.3		95.2	93.5						
			91.6		91.6						
			84.0		84.0			720	720	604	72.1
			CONS/COMMENTS							•••	
	** PROBL	ENS/ SULUT									
			DURING NOVEMBE			אדוא ס	CEILC	OTE COR	ALINE !	505 AR	LINER
.2/80		100.0									
	201	1.3	.0	.0	.0						
	301	100.0	98.8 88.1	100.0	98.8						
	401	100.0	88.1								
	SYSTEM	75.3	71.7	75.0	71.7			744	744	534	62.2
1/81	101	100.0	100.0	100.0	100.0						
	201	.0	.0 85.5 91.2	.0	.0						
	301	87.8	85.5	87.5	85.5						
	401	98.8	91.2 69.2	98.7	91.2						
	SYSTEM	71.7	69.2	71.6	69.2			744	744	533	56.1
	** PROBL	EMS/SOLUT	CONS/COMMENTS								
			THE UTILITY R			D-RELA	TED PR	OBLEMS	WERE EI	HCOUNTE	RED
			DURING DECEMBI	MAL UNA NE	JARY.						
2/81	101	95.3	-								
2/81	101 201	95.3 74.9	86.6	94.8	86.6						
2/81	201	74.9	86.6 73.6	94.8 74.6	86.6 73.6						
2/81	201	74.9	86.6 73.6	94.8 74.6	86.6 73.6						
2/81	201 301 401	74.9 28.4 100.0	86.6 73.6 23.8 93.1	94.8 74.6 24.9 100.0	86.6 73.6 23.8 93.1			672	672	466	47.9
2/81	201 301 401 SYSTEM	74.9 28.4 100.0 74.7	86.6 73.6 23.8 93.1 69.3	94.8 74.6 24.9 100.0	86.6 73.6			672	672	466	47.9
2/81	201 301 401 SYSTEM	74.9 28.4 100.0 74.7	86.6 73.6 23.8 93.1 69.3	94.8 74.6 24.9 100.0 73.6	86.6 73.6 23.8 93.1 69.3						
2/81	201 301 401 SYSTEM	74.9 28.4 100.0 74.7	86.6 73.6 23.8 93.1 69.3	94.8 74.6 24.9 100.0 73.6 RY A ROUTIN	86.6 73.6 23.8 93.1 69.3			REVEAL	_ED DET	ERIORAI	LION
	201 301 401 SYSTEM ** PROBL	74.9 28.4 100.0 74.7	86.6 73.6 23.8 93.1 69.3 IONS/COMMENTS DURING FEBRUAL OF THE ACID-RI	94.8 74.6 24.9 100.0 73.6 RY A ROUTIN	86.6 73.6 23.8 93.1 69.3			REVEAL	_ED DET	ERIORAI	LION
2/81	201 301 401 SYSTEM ** PROBL	74.9 28.4 100.0 74.7 EMS/SOLUT	86.6 73.6 23.8 93.1 69.3 IONS/COMMENTS DURING FEBRUAL OF THE ACID-RI	94.8 74.6 24.9 100.0 73.6 RY A ROUTIN	86.6 73.6 23.8 93.1 69.3 RE INSPECTION RICK AND MORTA			REVEAL	_ED DET	ERIORAI	LION
	201 301 401 SYSTEM ** PROBL	74.9 28.4 100.0 74.7 EMS/SOLUT:	86.6 73.6 23.8 93.1 69.3 IONS/COMMENTS DURING FEBRUAL OF THE ACID-RI IN THE NEAR FO	94.8 74.6 24.9 100.0 73.6 RY A ROUTIN ESISTANT BR JTURE.	86.6 73.6 23.8 93.1 69.3 NE INSPECTION RICK AND MORTAL			REVEAL	_ED DET	ERIORAI	LION
	201 301 401 SYSTEM ** PROBL	74.9 28.4 100.0 74.7 EMS/SOLUT: 97.2 99.1	86.6 73.6 23.8 93.1 69.3 IONS/COMMENTS DURING FEBRUAL OF THE ACID-RI IN THE NEAR FI 97.2 99.1 .0	94.8 74.6 24.9 100.0 73.6 RY A ROUTIN ESISTANT BE JTURE. 97.2 99.1	86.6 73.6 23.8 93.1 69.3 NE INSPECTION RICK AND MORTAL			REVEAL	_ED DET	ERIORAI	LION
	201 301 401 SYSTEM ** PROBL	74.9 28.4 100.0 74.7 EMS/SOLUT: 97.2 99.1	86.6 73.6 23.8 93.1 69.3 IONS/COMMENTS DURING FEBRUAI OF THE ACID-RI IN THE NEAR FI	94.8 74.6 24.9 100.0 73.6 RY A ROUTIN ESISTANT BE JTURE. 97.2 99.1	86.6 73.6 23.8 93.1 69.3 NE INSPECTION RICK AND MORTAL			REVEAL	_ED DET	ERIORAT REPLAC	LION
3/81	201 301 401 SYSTEM ** PROBL 101 201 301 401 SYSTEM	74.9 28.4 100.0 74.7 EMS/SOLUT: 97.2 99.1 .0 96.7	86.6 73.6 23.8 93.1 69.3 IONS/COMMENTS DURING FEBRUAL OF THE ACID-RI IN THE NEAR FO 97.2 99.1 .0 96.7	94.8 74.6 24.9 100.0 73.6 RY A ROUTIN ESISTANT BE JTURE. 97.2 99.1 .0 96.7	86.6 73.6 23.8 93.1 69.3 NE INSPECTION RICK AND MORTAL 97.2 99.1 .0 96.7			REVEAL L NECES	LED DET SSITATE	ERIORAT REPLAC	TION CEMENT
3/81	201 301 401 SYSTEM ** PROBL 101 201 301 401 SYSTEM	74.9 28.4 100.0 74.7 EMS/SOLUT: 97.2 99.1 .0 96.7 73.3	86.6 73.6 23.8 93.1 69.3 IONS/COMMENTS DURING FEBRUAL OF THE ACID-RI IN THE NEAR FO 97.2 99.1 .0 96.7 73.3	94.8 74.6 24.9 100.0 73.6 RY A ROUTIN ESISTANT BE JTURE. 97.2 99.1 .0 96.7 73.3	86.6 73.6 23.8 93.1 69.3 NE INSPECTION RICK AND MORTAL 97.2 99.1 .0 96.7 73.3			REVEAL L NECES	LED DET SSITATE	ERIORAT REPLAC	TION CEMENT
3/81	201 301 401 SYSTEM ** PROBL 101 201 301 401 SYSTEM 101 201	74.9 28.4 100.0 74.7 EMS/SOLUTE 97.2 99.1 .0 96.7 73.3	86.6 73.6 23.8 93.1 69.3 IONS/COMMENTS DURING FEBRUAL OF THE ACID-RI IN THE NEAR FO 97.2 99.1 .0 96.7 73.3	94.8 74.6 24.9 100.0 73.6 RY A ROUTIN ESISTANT BE JTURE. 97.2 99.1 .0 96.7 73.3	86.6 73.6 23.8 93.1 69.3 NE INSPECTION PICK AND MORTAL 97.2 99.1 .0 96.7 73.3			REVEAL L NECES	LED DET SSITATE	ERIORAT REPLAC	TION CEMENT
3/81	201 301 401 SYSTEM ** PROBL 101 201 301 401 SYSTEM 101 201 301	74.9 28.4 100.0 74.7 EMS/SOLUT: 97.2 99.1 .0 96.7 73.3 93.9 98.5 18.5	86.6 73.6 23.8 93.1 69.3 IONS/COMMENTS DURING FEBRUAL OF THE ACID-RI IN THE NEAR FO 97.2 99.1 .0 96.7 73.3 81.0 97.2 18.5	94.8 74.6 24.9 100.0 73.6 RY A ROUTIN ESISTANT BE JTURE. 97.2 99.1 .0 96.7 73.3 92.9 98.5 18.5	86.6 73.6 23.8 93.1 69.3 NE INSPECTION 97.2 97.2 97.1 .0 96.7 73.3 81.0 97.2 18.5			REVEAL L NECES	LED DET SSITATE	ERIORAT REPLAC	TION CEMENT
3/81	201 301 401 SYSTEM ** PROBL 101 201 301 401 SYSTEM 101 201	74.9 28.4 100.0 74.7 EMS/SOLUTE 97.2 99.1 .0 96.7 73.3 93.9 98.5	86.6 73.6 23.8 93.1 69.3 IONS/COMMENTS DURING FEBRUAL OF THE ACID-RI IN THE NEAR FO 97.2 99.1 .0 96.7 73.3	94.8 74.6 24.9 100.0 73.6 RY A ROUTIN ESISTANT BE JTURE. 97.2 99.1 .0 96.7 73.3	86.6 73.6 23.8 93.1 69.3 NE INSPECTION 97.2 97.2 97.1 .0 96.7 73.3 81.0 97.2			REVEAL L NECES	LED DET SSITATE	ERIORAT REPLAC 545	TION CEMENT 72.8
3/81 4/81	201 301 401 SYSTEM ** PROBL 101 201 301 401 SYSTEM 101 201 301 401 SYSTEM	74.9 28.4 100.0 74.7 EMS/SOLUT: 97.2 99.1 .0 96.7 73.3 93.9 98.5 18.5 82.3 73.3	86.6 73.6 23.8 93.1 69.3 IONS/COMMENTS DURING FEBRUAL OF THE ACID-RI IN THE NEAR FO 97.2 99.1 .0 96.7 73.3 81.0 97.2 18.5 82.3 69.8	94.8 74.6 24.9 100.0 73.6 RY A ROUTIN ESISTANT BR JTURE. 97.2 99.1 .0 96.7 73.3 92.9 98.5 18.5 82.3 73.1	86.6 73.6 23.8 93.1 69.3 NE INSPECTION 1 87.2 97.2 99.1 .0 96.7 73.3 81.0 97.2 18.5 82.3 69.8			REVEAL L NECES	LED DET SSITATE	ERIORAT REPLAC 545	TION CEMENT 72.8
3/81 4/81	201 301 401 SYSTEM ** PROBL 101 201 301 401 SYSTEM 101 SYSTEM 101	74.9 28.4 100.0 74.7 EMS/SOLUT: 97.2 99.1 .0 96.7 73.3 93.9 98.5 18.5 82.3 73.3	86.6 73.6 23.8 93.1 69.3 IONS/COMMENTS DURING FEBRUAL OF THE ACID-RI IN THE NEAR FO 97.2 99.1 .0 96.7 73.3 81.0 97.2 18.5 82.3 69.8	94.8 74.6 24.9 100.0 73.6 RY A ROUTIN ESISTANT BR JTURE. 97.2 99.1 .0 96.7 73.3 92.9 98.5 18.5 82.3 73.1	86.6 73.6 23.8 93.1 69.3 NE INSPECTION 1 PICK AND MORTAL 97.2 99.1 .0 96.7 73.3 81.0 97.2 18.5 82.3 69.8			REVEAL L NECES	LED DET SSITATE	ERIORAT REPLAC 545	TION CEMENT 72.8
3/81 4/81	201 301 401 SYSTEM ** PROBL 101 201 301 401 SYSTEM 101 201 301 401 SYSTEM 101 201	74.9 28.4 100.0 74.7 EMS/SOLUT: 97.2 99.1 .0 96.7 73.3 93.9 98.5 18.5 82.3 73.3	86.6 73.6 23.8 93.1 69.3 IONS/COMMENTS DURING FEBRUAL OF THE ACID-RI IN THE NEAR FO 97.2 99.1 .0 96.7 73.3 81.0 97.2 18.5 82.3 69.8	94.8 74.6 24.9 100.0 73.6 RY A ROUTIN ESISTANT BE JTURE. 97.2 99.1 .0 96.7 73.3 92.9 98.5 18.5 82.3 73.1	86.6 73.6 23.8 93.1 69.3 NE INSPECTION PRICK AND MORTAL 97.2 99.1 .0 96.7 73.3 81.0 97.2 18.5 82.3 69.8			REVEAL L NECES	LED DET SSITATE	ERIORAT REPLAC 545	TION CEMENT 72.8
3/81	201 301 401 SYSTEM ** PROBL 101 201 301 401 SYSTEM 101 SYSTEM 101	74.9 28.4 100.0 74.7 EMS/SOLUT: 97.2 99.1 .0 96.7 73.3 93.9 98.5 18.5 82.3 73.3	86.6 73.6 23.8 93.1 69.3 IONS/COMMENTS DURING FEBRUAL OF THE ACID-RI IN THE NEAR FO 97.2 99.1 .0 96.7 73.3 81.0 97.2 18.5 82.3 69.8	94.8 74.6 24.9 100.0 73.6 RY A ROUTIN ESISTANT BR JTURE. 97.2 99.1 .0 96.7 73.3 92.9 98.5 18.5 82.3 73.1	86.6 73.6 23.8 93.1 69.3 NE INSPECTION 1 PICK AND MORTAL 97.2 99.1 .0 96.7 73.3 81.0 97.2 18.5 82.3 69.8			REVEAL L NECES	LED DET SSITATE	ERIORAT REPLAC 545	TION CEMENT

DUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING MARCH, APRIL, AND MAY.

DURING THE MONTH OF MAY, REPLACEMENT OF THE RUBBER-LINED CARBON STEEL HOUSING WITH INCOLEY 825 ON NUMBER 401 ID FAN WAS INITIATED. HOUSING REPLACEMENTS ON FANS 201 AND 301 HAVE BEEN COMPLETED.

SODIUM THIOSULFATE ADDITION WAS UTILIZED THROUGHOUT THE MONTHS OF MARCH, APRIL, AND MAY TO REDUCE SCALING ENHANCED BY HIGH EXCESS AIR REQUIREMENTS OF THE BOILERS.

6/81	101	100.0	97.9	100.0	97.9	
	201	100.0	95.7	100.0	95.7	
	301	100.0	98.1	100.0	98.1	
	401	. 0	.0	.0	.0	
	SYSTEM	75.0	72.9	75.0	72.9	720

### ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE 401 WAS OUT OF SERVICE DURING JUNE SO THAT THE FAN HOUSING COULD BE REPLACED WITH INCONEL.

720

525 68.0

7/81	101	97.7	97.0	97.7	97.0				
	201	98.3	93.1	98.0	93.1				
	301	97.8	96.4	97.8	96.4				
	401	.0	.0	. 0	.0				
	SYSTEM	73.5	71.6	73.4	71.6	744	744	533	69.8

### ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE 401 REMAINED OUT OF SERVICE DUE TO FAN REPAIRS AND GENERAL CLEANING.

8/81	101	87.0	75.0	83.9	67.7				
	201	90.2	74.1	87.1	66.9				
	301	87.0	87.9	85.9	79.4				
	401	35.5	18.9	20.9	17.1				
	SYSTEM	74.9	64.0	69.5	57.8	744	672	430	35.0

## ** PROBLEMS/SOLUTIONS/COMMENTS

PHILLIPS WAS SHUT DOWN FOR THREE DAYS IN AUGUST FOR A STACK AND FGD SYSTEM INSPECTION. THE PRELIMINARY REPORT INDICATED STACK DETERIORATION TO THE POINT OF DAMAGING THE STACK INTEGRITY. AS A RESULT, THE UTILITY PLANS TO PRESSURIZE THE ANNULUS.

9/81	101	71.1	58.6	67.0	58.6				
<i>,,</i> 01		/ 1 . 1	50.6	67.0	20.0				
	201	94.3	75.9	93.0	75.9				
	301	98.1	82.4	97.7	82.4				
	401	9.5	2.1	2.3	2.1				
	SYSTEM	68.2	54.7	65.0	54.7	720	720	394	30.0

# ** PROBLEMS/SOLUTIONS/COMMENTS

DURING SEPTEMBER MODULE 101 UNAVAILABLE TIME WAS DUE TO THE START OF AN OVERHAUL.

MODULE 401 WAS OUT OF SERVICE FOR MOST OF SEPTEMBER TO INSTALL A NEW EXTERNAL MIST ELIMINATOR (MUNTERS).

10/81 101 51.6 51.6 51.6 51.6

DUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)

				~~~~PERFORMAI	NCE DATA	 				
PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION		PER HOURS	BOILER HOURS		CAP. FACTOR
	201	96. 0	52.0	92.8	52.0					
	301	95.4	34.0	88.1	34.0					
	401	97.7	97.7	97.7	97.7					
	SYSTEM	85.2	58.8	82.6	58.8		744	744	440	26.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE CEILCOTE LINERS IN MODULES 101 AND 201 WERE REPLACED WITH COROLINE 505 DURING OCTOBER.

DURING OCTOBER THE UTILITY INSTALLED SO2 MONITORS. TO DATE, THE MONITORS HAVE AN EXCELLENT PERFORMANCE RECORD.

11/81	101	.0	.0	.0	.0				
	201	98.3	27.8	95.7	37.8				
	301	97.7	25.4	91.8	25.4				
	401	100.0	100.0	100.0	100.0				
	SYSTEM	74.0	40.8	71.9	40.8	720	720	294	25.8

** PROBLEMS/SOLUTIONS/COMMENTS

DUE TO LOAD FLUCTUATIONS, MODULES 201 AND 301 WERE DOWN APPROXIMATELY 12 HOURS TO UNPLUG THE TANGENTIAL NOZZLES.

12/81	101	.0	.0	.0	.0				
	201	100.0	64.6	100.0	64.6				
	301	100.0	37.7	100.0	37. 7				
	401	93.6	93.6	93.6	93.6				
	SYSTEM	73.4	49.0	73.4	49.0	744	744	3 65	33.0

** PROBLEMS/SOLUTIONS/COMMENTS

MODULE 101 WAS OFF-LINE FOR THE ENTIRE PERIOD TO REPLACE THE RUBBER LINED FAN HOUSING WITH INCONEL 825 AND TO INSTALL NEW STUDS IN THE FAN ROTOR.

DURING NOVEMBER AND DECEMBER MODULE 101 WAS OFF-LINE FOR CLEANING. THE MODULE OPERATED 6,487 HOURS BEFORE BEING SHUT DOWN.

1/82	101	.0	. 0	.0	.0				
	201	100.0	80.9	100.0	80.9				
	301	90.2	88.9	90.1	88.9				
	401	95.6	95.6	95.6	95.6				
	SYSTEM	71.5	66.3	69.9	66.3	744	744	494	64.0
2/82	101	. 0	.0	. 0	.0				
	201	99.2	64.0	98.8	64.0				
	301	100.0	80.4	100.0	80.4				
	401	100.0	100.0	100.0	100.0				
	SYSTEM	74.8	61.1	70.8	61.1	672	672	411	60.0
3/82	101	.0	.0	. 0	. 0				
	201	99.1	57.3	98.4	57.3				
	301	100.0	79.7	100.0	79.7				
	401	100.0	99.6	100.0	99.6				
	SYSTEM	74.8	59.1	70.1	59.1	744	744	440	46.0

** PROBLEMS/SOLUTIONS/COMMENTS

MODULE 101 WAS OFF-LINE THE ENTIRE FIRST QUARTER OF 1982 FOR REPAIRS.

NEW SO2 MONITORS, INSTALLED IN JANUARY, WERE REPORTED TO HAVE WORKED WELL THROUGHOUT THE FIRST QUARTER. THE UTILITY IS ALSO PRESENTLY REQUESTING/EVALUATING BIDS TO PRESSURIZE THE STACK ANNULUS.

DUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)

			 PERFORMA	NCE DATA				 	
		AVAILABILITY			% RE	MOVAL	PER	FGD	CAP.
4/82	SYSTEM						720		
5/82	SYSTEM						744		
6/82	SYSTEM						720		

** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE SECOND QUARTER THE SO2 MONITORS WERE CERTIFIED.

THE MODULE 301 MIST ELIMINATOR WAS REPLACED DUE TO DETERIORATION.

THE MODULE 401 FAN HAD TO BE BALANCED DURING THE PERIOD CAUSING ADDITIONAL OUTAGE TIME.

DURING THE PERIOD THE UTILITY INITIATED ADDING THIOSULFATE WHEN THE EXCESS AIR RECORDED GREATER THAN 11. THIS HAS SOLVED SOME OF THERE PREVIOUS PROBLEMS.

7 /82	SYSTEM	744
8/82	SYSTEM	744
9/82	SYSTEM	720
10/82	SYSTEM	744
11/82	SYSTEM	720
12/82	SYSTEM	744
1/83	SYSTEM	744
2/83	SYSTEM	672
3/83	SYSTEM	744

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE PERIOD OF JULY 1982 THROUGH MARCH 1983.

4/83	SYSTEM		720
5/83	SYSTEM	-	744
6/83	SYSTEM		72 ft

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY INITIATED STACK PRESSURIZATION AT PHILLIPS DURING THE MONTH TO CONTROL SEEPAGE AND SUBSEQUENT CORROSION.

7/83	SYSTEM	744
8/83	SYSTEM	744
9/83	SYSTEM	720

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE THIRD QUARTER OF 1983.

10/83 SYSTEM 744

DUQUESNE LIGHT: PHILLIPS 1-6 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

11/83 SYSTEM

720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED INCREASING STACK PRESSURE BY TWO INCHES DURING THE MONTH FOR CONTROL OF SEEPAGE.

12/83 SYSTEM

744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT ALTHOUGH THE UNIT HAS BEEN DOWN MONTHS AT A TIME DURING MOST OF 1983, THE FGD SYSTEM HAS BEEN AVAILABLE.

STAINLESS STEEL BANDS AROUND THE ABSORBER LINER WERE REPLACED WITH NARCOLITE DURING THE FOURTH QUARTER.

INSPECTIONS INDICATE THAT THE CEILCOTE LINING IN THE WET DUCT WILL HAVE TO BE REPLACED OVER THE NEXT THREE YEARS.

1/84 SYST	TEM	744
2/84 SYST	TEM	696
3/84 SYST	тем	744
4/84 SYST	TEM	720
5/84 SYST	тем	744
6/84 SYST	тем	720
7/84 SYST	тем	744
8/84 SYST	TEM	744
9/84 SYST	тен -	720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT OVERALL FGD SYSTEM AVAILABILITY FOR THE FIRST THREE QUARTERS OF 1984 WAS ABOVE 90%.

IT WAS REPORTED THAT LESS DETERIORATION HAS OCCURRED IN THE STACK NOW THAT IT IS PRESSURIZED.

AFTER 11 YEARS OF USAGE, THE CEILCOTE LINER IN THE WET DUCT TO THE STACK DETERIORATED. THE LINER WILL BE REPLACED OVER THE NEXT THREE YEARS DURING ANNUAL OUTAGES.

THE UTILITY IS NOW DIVERTING INDUCED DRAFT FAN SPRAY WATER TO AN ASH POND INSTEAD OF RECYCLING TO THE ABSORBERS. LIME CONSUMPTION HAS IMPROVED SINCE THE HIGHLY ACIDIC SPRAY WATER IS NO LONGER INTRODUCED IN THE SYSTEM.

THE UTILITY REPORTED A THREE WEEK SCHEDULED ANNUAL OUTAGE IN THE FIRST THREE QUARTERS OF 1984. DURING THIS TIME REPAIRS WERE MADE TO DUCTWORK AND DAMPERS. MIST ELIMINATOR TURN VANES WERE ALSO REPLACED.

DUE TO LOW POWER DEMAND IN THE FIRST THREE QUARTERS OF 1984, PHILLIPS DID NOT OPERATE STEADILY. AS A RESULT, BRIEF EPISODES OF HIGH EMISSIONS WERE REPORTED. HOWEVER, THE SYSTEM OPERATED EFFICIENTLY OVER 24 HOUR PERIODS.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

EAST KENTUCKY POWER COMPANY NAME SPURLOCK PLANT NAME UNIT NUMBER MAYSVILLE CITY KENTUCKY STATE REGULATORY CLASSIFICATION 43. 516. ***** (.100 LB/MMBTU) (1.200 LB/MMBTU) (****** LB/MMBTU) PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J 800 500 NET PLANT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW NET UNIT GENERATING CAPACITY W/FGD - MW 500 NET UNIT GENERATING CAPACITY W/FGD - MW NET UNIT GENERATING CAPACITY HO/FGD - MW 495 EQUIVALENT SCRUBBED CAPACITY - MW 500 ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER COMBUSTION ENGINEERING BOILER TYPE PULVERIZED COAL BOILER SERVICE LOAD BASE DESIGN BOILER FLUE GAS FLOW - CU.M/S
BOILER FLUE GAS TEMPERATURE - C
STACK HEIGHT - M ***** ****** (****** ACFM)
148.9 (300 F)
244. (802 FT) STACK HEIGHT - M STACK SHELL CONCRETE STACK TOP DIAMETER - M 9.1 (30.0 FT) ** FUEL DATA FUEL TYPE COAL FUEL GRADE ***** AVERAGE HEAT CONTENT - J/G 25586. (11000 BTU/LB) RANGE HEAT CONTENT - BTU/LB ***** AVERAGE ASH CONTENT - % 16.00 RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT % 8.00 RANGE MOISTURE CONTENT - % AVERAGE SULFUR CONTENT - % 3.50 RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % ****** RANGE CHLORIDE CONTENT - % 0.02-0.11 *** PARTICLE CONTROL ** ESP TYPE HOT SIDE SUPPLIER AMERICAN AIR FILTER PARTICLE REMOVAL EFFICENCY - % 99.5 ** PARTICLE SCRUBBER NUMBER GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL N/A LINER GENERIC MATERIAL N/A LINER SPECIFIC MATERIAL N/A GAS CONTACTING DEVICE TYPE N/A *** FGD SYSTEM ** GENERAL DATA SALEABLE PRODUCT/THROWAWAY PRODUCT THROWAWAY PRODUCT SO2 REMOVAL MODE WET SCRUBBING PROCESS TYPE LIME SYSTEM SUPPLIER THYSSEN/CEA A-E FIRM BLACK & VEATCH DEVELOPMENT LEVEL FULL SCALE NEW/RETROFIT UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.50 UNIT DESIGN SO2 REMOVAL EFFICIENCY - % 79.40

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EAST KENTUCKY POWER: SPURLOCK 2 (CONT.)
    CURRENT STATUS
                                                  4/83
    COMMERCIAL START-UP
    INITIAL START-UP
                                                 12/82
                                                  0/79
    CONTRACT AHARDED
 ** DESIGN AND OPERATING PARAMETERS
    OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                   120.0
 ** QUENCHER/PRESATURATOR
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                 ND
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                 NR
 ** ABSORBER
    NUMBER
    GENERIC TYPE
                                                 SPRAY TOWER
    SPECIFIC TYPE
                                                 OPEN COUNTERCURRENT SPRAY
    TRADE NAME/COMMON TYPE
                                                 N/A
    SHELL GENERIC MATERIAL
                                                 NR
    SHELL SPECIFIC MATERIAL
                                                 NR
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                                 NR
    LINER GENERIC MATERIAL
                                                 NR
    LINER SPECIFIC MATERIAL
                                                 NR
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                                 ΝR
    GAS CONTACTING DEVICE TYPE
                                                 NONE
    NUMBER OF CONTACTING ZONES
                                                  1
    L/G RATIO - L/CU.M
                                                                 ( 10.0 GAL/1000 ACF)
                                                      1.3
    GAS-SIDE PRESSURE DROP - KPA
                                                                 ( 5.8 IN-H20)
                                                     1.4
    SO2 REMOVAL EFFICIENCY - %
                                                     90.0
 ** MIST ELIMINATOR
    PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                                 PRIMARY COLLECTOR
    NUMBER PER SYSTEM
    GENERIC TYPE
                                                  IMPINGEMENT
    SPECIFIC TYPE
                                                 BAFFLE
    TRADE NAME/COMMON TYPE
                                                 CLOSED VANE
    NUMBER OF PASSES PER STAGE
                                                      4
    PRESSURE DROP - KPA
                                                       .0
                                                                 ( .1 IN-H20)
    SUPERFICAL GAS VELOCITY - M/S
                                                                 ( 1.0 FT/S)
                                                       . 3
                                                 ORGANIC
    CONSTRUCTION MATERIAL GENERIC TYPE
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                 POLYPHENYLENE
    WASH FREQUENCY
                                                 CONTINUOUS
 ** REHEATER
    NUMBER
                                                  1
                                                  INDIRECT HOT AIR
    GENERIC TYPE
    SPECIFIC TYPE
                                                  COLD SIDE
    TRADE NAME/COMMON TYPE
                                                 N/A
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                 NR
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                 NR
 ** FANS
    NUMBER
                                                  2
    DESIGN
                                                  CENTRIFUGAL
    FUNCTION
                                                 NR
    APPLICATION
                                                  FORCED DRAFT
    SERVICE
                                                 DRY
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                 HIGH ALLOY
 ** FANS
    NUMBER
                                                  6
    DESIGN
                                                  CENTRIFUGAL
    FUNCTION
                                                 NR
    APPLICATION
                                                  FORCED DRAFT
    SERVICE
                                                 DRY
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                 HIGH ALLOY
 ** DAMPERS
    FUNCTION
                                                 NR
    GENERIC TYPE
                                                 NR
    SPECIFIC TYPE
                                                 NR
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                  NR
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UTILITY FGD SURVEY: OCTOBER 1983 - SEPTEMBER 1984 EAST KENTUCKY POWER: SPURLOCK 2 (CONT.) NR CONSTRUCTION MATERIAL SPECIFIC TYPE NR LINER GENERIC MATERIAL TYPE NR LINER SPECIFIC MATERIAL TYPE ** DUCTWORK SHELL GENERIC MATERIAL TYPE ΝR NR SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE NR NR LINER SPECIFIC MATERIAL TYPE ** REAGENT PREPARATION EQUIPMENT SLAKER FUNCTION NR DEVICE NR DEVICE TYPE ** TANKS NUMBER SERVICE ABSORBER RECYCLE REAGENT PREP PRODUCT **** ** PUMPS NUMBER SERVICE -----SLURRY TRANSFER ** SOLIDS CONCENTRATING/DEWATERING THICKENER DEVICE 2 NUMBER 115.0 DIA DIMENSIONS - FT SHELL GENERIC MATERIAL TYPE CARBON STEEL SHELL SPECIFIC MATERIAL TYPE AISI 1110 30% SOLIDS OUTLET STREAM CHARACTERISTICS *** SLUDGE ** TREATMENT FIXATION METHOD DEVICE PUG MILL CONVERSION SYSTEMS [POZ-O-TEC] PROPRIETARY PROCESS ** DISFOSAL FINAL NATURE TYPE ΝR SITE TRANSPORTATION METHOD RAIL SITE TREATMENT NR ** WATER BALANCE WATER LOOP TYPE CLOSED

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

12/82 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT INITIAL START-UP OCCURRED IN DECEMBER, 1982.

 1/83
 SYSTEM
 744

 2/83
 SYSTEM
 672

 3/83
 SYSTEM
 744

FAST KENTUCKY POWER: SPURLOCK 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT SO FAR THE FGD SYSTEM IS OPERATING AT ABOUT 90% EFFICIENCY WITH NO MAJOR PROBLEMS.

4/83	SYSTEM	720
5/83	SYSTEM	744
6/83	SYSTEM	720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY ANNOUNCED THAT THE SPURLOCK 2 FGD SYSTEM INITIATED COMMERICAL OPERATION IN APRIL. PEFORMANCE DATA FOR THE PERIOD OF APRIL THROUGH JUNE 1983, ARE NOT AVAILABLE AT THIS TIME.

7/83	SYSTEM	.0	.0	744	0
8/83	SYSTEM	.0	.0	744	0
9/83	SYSTEM	.0	.0	720	0

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE FGD SYSTEM WAS OUT OF SERVICE DURING THE THIRD QUARTER DUE TO DUCTWORK PROBLEMS.

STACK-RELATED PROBLEMS WERE ALSO REPORTED DURING THE PERIOD.

THE UTILITY HOPES TO RESUME OPERATION OF THE SPURLOCK 2 FGD SYSTEM DURING THE FIRST QUARTER OF 1984.

10/	3 SYSTEM	744
11/	33 SYSTEM	720
12/	3 SYSTEM	744

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS REPORTED APPROXIMATELY 90 PERCENT AVAILABLE THROUGHOUT THE FOURTH QUARTER OF 1983.

THE UTILITY REPORTED THAT THE UNIT WAS DOWN FROM MID-NOVEMBER TO LATE DECEMBER DUE TO STACK AND DUCTWORK-RELATED PROBLEMS.

1/84	SYSTEM	744
2/84	SYSTEM	696
3/84	SYSTEM	744
4/84	SYSTEM	720
5/84	SYSTEM	744
6/84	SYSTEM	720
7/84	SYSTEM	744
8/84	SYSTEM	744
9/84	SYSTEM	720

EAST KENTUCKY POWER: SPURLOCK 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE FGD SYSTEM WAS OUT OF SERVICE DURING THE FIRST THREE QUARTERS OF 1984 AND IS SCHEDULED TO GO BACK ON LINE BY LATE DECEMBER 1984. THE SYSTEM WAS DOWN DUE TO STACK LINER REPLACEMENT AND ABSORBER DUCTWORK REPAIRS.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

_____ GRAND HAVEN BRD OF LIGHT & PWR COMPANY NAME PLANT NAME J.B. SIMS UNIT NUMBER GRAND HAVEN CITY MICHIGAN STATE REGULATORY CLASSIFICATION PARTICULATE EMISSION LIMITATION - NG/J 13. 516. ***** (.030 LB/MMBTU) SO2 EMISSION LIMITATION - NG/J (1.200 LB/MMBTU) (***** LB/MMBTU) NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW 78 GROSS UNIT GENERATING CAPACITY - MW 65 GROSS UNIT GENERATING CAPACITY - MW
NET UNIT GENERATING CAPACITY W/FGD - MW
NET UNIT GENERATING CAPACITY WO/FGD - MW 58 58 495 EQUIVALENT SCRUBBED CAPACITY - MW 65 ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER BABCOCK & WILCOX BOILER TYPE PULVERIZED COAL BASE 122.69 142.8 110. CONCRETE 2.6 BOILER SERVICE LOAD DESIGN BOILER FLUE GAS FLOW - CU.M/S (260000 ACFM) BOILER FLUE GAS TEMPERATURE + C (289 F) STACK HEIGHT - M (360 FT) STACK SHELL STACK TOP DIAMETER - M (8.5 FT) ** FUEL DATA FUEL TYPE COAL FUEL GRADE BITUMINOUS AVERAGE HEAT CONTENT - J/G 25586. (11000 BTU/LB) RANGE HEAT CONTENT - BTU/LB 10700-12265 11.20 AVERAGE ASH CONTENT - % 9.5-15.8 RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - % 9.60 RANGE MOISTURE CONTENT - % 3.3-15.5 AVERAGE SULFUR CONTENT - % 2.75 RANGE SULFUR CONTENT - % 1.2-4.5 AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - % **** *** PARTICLE CONTROL ** ESP NUMBER 1 COLD SIDE TYPE SUPPLIER BABCOCK & WILCOX 127.4 (270000 ACFM) 140.6 (285 F) .1 (0. IN-H20) INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE - C PRESSURE DROP - KPA ** PARTICLE SCRUSBER NUMBER 0 GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL N/A LINER GENERIC MATERIAL N/A LINER SPECIFIC MATERIAL N/A *** FGD SYSTEM ** GENERAL DATA SALEABLE PRODUCT/THROWAWAY PRODUCT THROWAWAY PRODUCT SO2 REMOVAL MODE WET SCRUBBING PROCESS TYPE LIME BAECOCK & WILCOX SYSTEM SUPPLIER BLACK & VEATCH A-E FIRM DEVELOPMENT LEVEL FULL SCALE

NEW

NEW/RETROFIT

```
GRAND HAVEN BRD OF LIGHT & PWR: J.B. SIMS 3 (CONT.)
```

```
UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                 90.00
                                               1
   CURRENT STATUS
                                               8/83
   COMMERCIAL START-UP
                                               5/83
   INITIAL START-UP
                                              12/79
   CONTRACT AWARDED
** DESIGN AND OPERATING PARAMETERS
** QUENCHER/PRESATURATOR
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              NR
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                             ΝŔ
** ABSORBER
                                               2
   NUMBER
   NUMBER OF SPARES
                                               1
                                              SPRAY TOWER
   GENERIC TYPE
   SPECIFIC TYPE
                                              OPEN COUNTERCURRENT SPRAY
    TRADE NAME/COMMON TYPE
                                              N/A
                                              BABCOCK & WILCOX
   SUPPLIER.
                                              25.0 DIA X 95.0
   DIMENSIONS - FT
    SHELL GENERIC MATERIAL
                                              STAINLESS STEEL
    SHELL SPECIFIC MATERIAL
                                              AUSTENITIC
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                              TYPE 316L
    LINER GENERIC MATERIAL
                                              NONE
    LINER SPECIFIC MATERIAL
                                              N/A
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                              N/A
    NUMBER OF CONTACTING ZONES
                                               4
    LIQUID RECIRCULATION RATE - LITER/S
                                               1180.
                                                           (18737 GPM)
                                               11.8
                                                            ( 88.0 GAL/1000 ACF)
    L/G RATTO L/CU.M.
    GAS-SIDE PRESSURE DROP - KPA
                                                1.4
                                                            ( 5.4 IN-H2O)
    INLET GAS FLOW - CU. M/S
                                                122.69
                                                            ( 260000 ACFM)
    INLET GAS TEMPERATURE C
                                               140.6
                                                            ( 285 F)
    SO2 REMOVAL EFFICIENCY - %
                                                 90.0
** MIST ELIMINATOR
   PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                              PRIMARY COLLECTOR
    NUMBER PER SYSTEM
                                              IMPINGEMENT
   GENERIC TYPE
    SPECIFIC TYPE
                                              BAFFLE
    TRADE NAME/COMMON TYPE
                                              CLOSED VANE
    CONFIGURATION
                                              VERTICAL
   NUMBER OF STAGES
    NUMBER OF PASSES PER STAGE
                                                  3
    CONSTRUCTION MATERIAL GENERIC TYPE
                                              ORGANIC
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                             FIBER-REINFORCED POLYESTER
   WASH WATER SOURCE
                                              BLENDED
   WASH RATE - L/S
                                                 6.6
                                                           ( 104 GAL/MIN)
** REHEATER
   NUMBER
    GENERIC TYPE
                                              IN-LINE
    SPECIFIC TYPE
                                              HOT WATER -
    TRADE NAME/COMMON TYPE
    PERCENT GAS BYPASSED - AVG
TEMPERATURE INCREASE C
                                                  .0
                                                 27.8
                                                            ( 50 F)
    INLET FLUE GAS FLOW RATE - CU. M/S
                                              122.69
                                                            ( 260000 ACFM)
    INLET FLUE GAS TEMPERATURE C
                                               50.6
                                                            ( 123 F)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                              ΝR
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              NR
** FANS
   NUMBER
                                               2
   NUMBER OF SPARES
                                               0
    DESIGN
                                              NR
    FUNCTION
                                              BALANCED DRAFT
    APPLICATION
                                              INDUCED DRAFT
    SERVICE
                                              DRY
    FLUE GAS FLOW RATE - CU.M/S
                                                69.37
                                                          ( 147000 ACFM)
   FLUE GAS TEMPERATURE C
                                               140.6
                                                             ( 285 F)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                            NR
```

GRAND HAVEN BRD OF LIGHT & PWR: J.B. SIMS 3 (CONT.)

```
** FANS
   NUMBER
                                                 2
   NUMBER OF SPARES
                                                 ۵
                                                NR
   DESTON
                                                BALANCED DRAFT
    FUNCTION
    APPLICATION
                                                FORCED DRAFT
    SERVICE
                                                DRY
    FLUE GAS FLOW RATE - CU.M/S
                                                   49.08
                                                                ( 104000 ACFM)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                CARBON STEEL
** DAMPERS
                                                NR
   FUNCTION
    GENERIC TYPE
                                                NR
    SPECIFIC TYPE
                                                NR
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                NR
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                NΩ
    LINER GENERIC MATERIAL TYPE
                                                NR
    LINER SPECIFIC MATERIAL TYPE
                                                ND
** DUCTWORK
     SHELL GENERIC MATERIAL TYPE
                                                NR
     SHELL SPECIFIC MATERIAL TYPE
                                                NR
     LINER GENERIC MATERIAL TYPE
                                                NR
     LINER SPECIFIC MATERIAL TYPE
                                                NR
** REAGENT PREPARATION EQUIPMENT
    FUNCTION
                                                SLAKER
    DEVICE
                                                NR
    DEVICE TYPE
                                                NR
    NUMBER
                                                 2
** TANKS
    SERVICE
                                                NUMBER
                                                                           .ت
    -----
                                                 -----
    ABSORBER RECYCLE
                                                   1
    REAGENT PREP PRODUCT
                                                    1
    SPARGER/OXIDIZER
** PUMPS
    SERVICE
                                                NUMBER
    LIME SLURRY TRANSFER
                                                   2
    SCRUBBER RECIRCULATION
                                                    6
    RECYCLE WATER
                                                   2
** SOLIDS CONCENTRATING/DEWATERING
    DEVICE
                                                THICKENER
    NUMBER
                                                 1
    NUMBER OF SPARES
                                                CIRCULAR
    CONFIGURATION
    DIMENSIONS - FT
                                                70.0 DIA X 14.0
                                                18% SOLIDS
    FEED STREAM CHARACTERISTICS
                                                35% SOLIDS
    OUTLET STREAM CHARACTERISTICS
** SOLIDS CONCENTRATING/DEWATERING
                                                VACUUM FILTER
    DEVICE
    NUMBER
                                                 2
    NUMBER OF SPARES
                                                1
    FEED STREAM CHARACTERISTICS
                                                35% SOLIDS
    OUTLET STREAM CHARACTERISTICS
                                                63% SOLIDS
*** SLUDGE
** TREATMENT
   METHOD
                                                FIXATION
    DEVICE
                                                PUG MILL
    PROPRIETARY PROCESS
                                                N/A
   INLET FLOW RATE - LITER/S
                                                    1.0
                                                                (
                                                                   16 GPM)
```

GRAND HAVEN BRD OF LIGHT & PWR: J.B. SIMS 3 (CONT.)

** DISPOSAL

NATURE FINAL LANDFILL LOCATION OFF-SITE

** PROCESS CONTROL AND INSTRUMENTATION CHEMICAL PARAMETERS

PROCESS CHEMISTRY MODE

PH, SLURRY DENSITY FEED FORWARD

** WATER BALANCE

WATER LOOP TYPE

CLOSED

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS HOURS FACTOR

5/83 SYSTEM

744

6/83 SYSTEM

720

** PROBLEMS/SOLUTIONS/COMMENTS

INITIAL START-UP AND SHAKEDOWN PROCEDURES OF THE FGD SYSTEM COMMENCED IN MAY. THE UNIT IS SCHEDULED TO BEGIN COMMERCIAL OPERATIONS BY JULY, 1983.

THE UTILITY REPORTED THAT NO MAJOR PROBLEMS WERE ENCOUNTERED DURING STARTUP WITH EITHER THE TURBINE OR FGD SYSTEM. INITIAL FGD PERFORMANCE TESTING SHOWED A 98 PERCENT SO2 REMOVAL EFFICIENCY.

SINCE STARTUP, THE UTILITY REPORTED THAT IT HAS ENCOUNTERD PROBLEMS WITH PROPER BOILER COMBUSTION.

7/83 SYSTEM 744 8/83 SYSTEM 744 9/83 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE FGD SYSTEM BEGAN COMMERCIAL OPERATIONS ON AUGUST 8, 1983. THE FGD SYSTEM HAS CONTINUED TO ACHIEVE HIGH SO2 REMOVAL EFFICIENCIES IN THE RANGE OF 90 TO 95%.
ALTHOUGH GAS SIDE OPERATION HAS BEEN EXCELLENT, THE UTILITY REPORTED THAT IT EXPERIENCED MINOR PROBLEMS WITH SYSTEM CHEMISTRY AND WASTE HANDLING.

THE FORCED OXIDATION SYSTEM HAS NOT OPERATED TO ITS DESIGNED CAPACITY. ALTHOUGH DESIGNED TO ACHIEVE BETWEEN 80 TO 90% OXIDATION, ACTUAL RATES HAVE BEEN IN THE RANGE OF 10 TO 35%. PLUGGED SPARGERS AND LOOSE DOWNCOMERS IN THE OXIDATION TANK ARE REPORTED TO BE THE CAUSE.

THE UTILITY REPORTED THAT THE SLUDGE HANDLING CONVEYORS WERE UNDERDESIGNED. THE UTILITY SOLVED THE PROBLEM BY INCREASING THE SPEED OF THE CONVEYORS.

MODULE A EXPERIENCED PLUGGED SPRAY NOZZLES DURING THE THIRD QUARTER. THE UTILITY REPORTED THAT MAINTENANCE WORKERS REMOVED HARD SCALE FROM THE INLET OF THE ABSORBER, AND CHUNKS OF SCALE DROPPED INTO THE ABSORBER SUMP. SUBSEQUENTLY, THE PUMPS PICKED UP THE SCALE AND FED IT TO THE NOZZLES CAUSING THEM TO PLUG.

PUMP ALIGNMENT PROBLEMS HAVE CAUSED SEVERAL BEARING FAILURES ON THE MODULE B ABSORBER.

MINOR PLUGGING PROBLEMS WERE ENCOUNTERED WITH THE PUG MILL DURING THE THIRD QUARTER.

10/83 SYSTEM

744

GRAND HAVEN BRD OF LIGHT & PWR: J.B. SIMS 3 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE FGD SYSTEM WAS FORCED OFF-LINE FOR 1.5 WEEKS IN OCTOBER TO MAKE REPAIRS TO THE FORCED OXIDATION TANK. A LOOSE DOWN-COMER IN THE TANK CAUSED DAMAGE TO THE STIR PADDLE AND RUBBER LINING.

11/83 SYSTEM 720 12/83 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURING THE MONTHS OF NOVEMBER AND DECEMBER. FGD SYSTEM AVAILABILITY DURING THESE TWO MONTHS WAS APPROXIMATELY 99 PERCENT. THE SYSTEM WAS REPORTED TO BE ACHIEVING SO2 REMOVAL EFFICIENCIES IN THE RANGE OF 95 TO 98 PERCENT.

1/84	SYSTEM	744
2/84	SYSTEM	696
3/84	SYSTEM	744
4/84	SYSTEM	720
5/84	SYSTEM	744
6/84	SYSTEM	720
7/84	SYSTEM	744
8/84	SYSTEM	744
9/84	SYSTEM	720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT A SECTION OF MIST ELIMINATOR CHEVRON BAFFLES FELL DURING THE THIRD QUARTER 1984.

THIOSORBIC LIME TESTING WAS CONDUCTED DURING THE FIRST THREE QUARTERS OF 1984.

FGD SYSTEM AVAILABILITY DURING THE FIRST THREE QUARTERS OF 1984 WAS ESTIMATED AT 99%.

THE UTILITY REPORTED THAT SO2 REMOVAL EFFICIENCIES DURING THE FIRST THREE QUARTERS OF 1984 WERE APPROXIMATELY 92 TO 97 PERCENT.

BABCOCK AND WILCOX IS INSTALLING A DUST COLLECTION SYSTEM AT THE SLUDGE-FLYASH MIXING AREA. EXCESSIVE DUST LEVELS FROM THE PUG MILLS WARRANTED THE DECISION TO INSTALL THIS EQUIPMENT.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

HOOSIER ENERGY COMPANY NAME MEROM PLANT NAME UNIT NUMBER MEROM CITY INDIANA STATE REGULATORY CLASSIFICATION D 43. (.100 LB/MMBTU) 516. (1.200 LB/MMBTU) ****** (****** LB/MMBTU) PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW **** 490 GROSS UNIT GENERATING CAPACITY - MW NET UNIT GENERATING CAPACITY W/FGD - MW 460 NET UNIT GENERATING CAPACITY WO/FGD - MW 466 EQUIVALENT SCRUBBED CAPACITY - MW 441 ** UNIT DATA - BOILER AND STACK RILEY STOKER BOILER SUPPLIER BOILER TYPE PULVERIZED COAL BOILER SERVICE LOAD BASE (1732000 ACFM) DESIGN EOILER FLUE GAS FLOW - CU.M/S 817.33 ****** 214. CONCRETE BOILER FLUE GAS TEMPERATURE - C (**** F) (702 FT) STACK HEIGHT - M STACK SHELL STACK TOP DIAMETER - M 5.8 (19.0 FT) ** FUEL DATA FUEL TYPE COAL FUEL GRADE BITUMINOUS AVERAGE HEAT CONTENT - J/G ***** (**** BTU/LB) RANGE HEAT CONTENT - BTU/LB ***** AVERAGE ASH CONTENT - % ***** RANGE ASH CONTENT - % ***** 3 AVERAGE MOISTURE CONTENT - % ***** RANGE MOISTURE CONTENT % ***** AVERAGE SULFUR CONTENT - % 3.50 RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % .20 RANGE CHLORIDE CONTENT - % *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER Λ TYPE NONE ** FABRIC FILTER NUMBER n TYPE NONE ** ESP NUMBER 1 NUMBER OF SPARES COLD SIDE SUPPLIER BUELL DIVISION, ENVIROTECH INLET FLUE GAS CAPACITY - CU.M/S 873.0 (1850000 ACFM) 137.8 (280 F) 137.8 INLET FLUE GAS TEMPERATURE - C PARTICLE REMOVAL EFFICENCY - % 99.4 ** PARTICLE SCRUBBER NUMBER GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL N/A LINER GENERIC MATERIAL N/A LINER SPECIFIC MATERIAL N/A GAS CONTACTING DEVICE TYPE N/A

HOOSIER ENERGY: MEROM 1 (CONT.)

*** FGD SYSTEM

```
** GENERAL DATA
                                               THROWAWAY PRODUCT
   SALEABLE PRODUCT/THROWAWAY PRODUCT
   SO2 REMOVAL MODE
                                               WET SCRUBBING
   PROCESS TYPE
                                               LIMESTONE
                                               MITSUBISHI HEAVY INDUSTRIES
   SYSTEM SUPPLIER
                                               UNITED ENGINEERS & CONSTRUCTORS
   A-E FIRM
   DEVELOPMENT LEVEL
                                               FULL SCALE
   NEW/RETROFIT
                                               NEM
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.40
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                  90.00
   ENERGY CONSUMPTION - %
                                                   1.2
   CURRENT STATUS
   COMMERCIAL START-UP
                                                8/82
   INITIAL START-UP
                                                8/82
   CONTRACT AWARDED
                                                3/78
** DESIGN AND OPERATING PARAMETERS
   DESIGN COAL SULFER CONTENT - %
                                                   4.20
    DESIGN COAL HEAT CONTENT - J/G
                                               24423.0
                                                               ( 10500 BTU/LB)
   DESIGN COAL ASH CONTENT - %
                                                  16.00
** QUENCHER/PRESATURATOR
    CONSTRUCTION MATERIAL GENERIC TYPE
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               NR
** ABSORBER
    NUMBER
                                                4
   NUMBER OF SPARES
                                                n
    GENERIC TYPE
                                               PACKED TOWER
    SPECIFIC TYPE
                                               GRID PACKING
                                               COCURRENT
    TRADE NAME/COMMON TYPE
    SUPPLIER
                                               MITSUBISHI
    SHELL GENERIC MATERIAL
                                               CARBON STEEL
    SHELL SPECIFIC MATERIAL
                                               NP
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                               NΒ
    LINER GENERIC MATERIAL
                                               ND
    LINER SPECIFIC MATERIAL
                                               NR
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                               NΒ
                                               FIXED GRIDS
    GAS CONTACTING DEVICE TYPE
                                                               (21160 GPM)
    LIQUID RECIRCULATION RATE - LITER/S
                                                1333.
    L/G RATIO - L/CU.M
                                                  5.7
                                                              ( 42.3 GAL/1000 ACF)
                                                  235.95
                                                              ( 500000 ACFM)
    INLET GAS FLOW - CU. M/S
                                                               ( 280 F)
    INLET GAS TEMPERATURE - C
                                                 137.8
    SO2 REMOVAL EFFICIENCY - %
                                                   90.0
** MIST ELIMINATOR
    PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                               MIST ELININATOR
    NUMBER PER SYSTEM
                                                4
    NUMBER OF SPARES PER SYSTEM
                                                 0
    NUMBER PER MODULE
                                                 1
    GENERIC TYPE
                                               NR
    SPECIFIC TYPE
                                               NR
    TRADE NAME/COMMON TYPE
                                               NR
    CONFIGURATION
                                               HORIZONTAL
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               NR
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               NR
** REHEATER
   NUMBER
                                                7
    GENERIC TYPE
                                                INDIRECT HOT AIR
    SPECIFIC TYPE
                                               ИR
    TRADE NAME/COMMON TYPE
                                               NR
                                                                 50 F)
    TEMPERATURE INCREASE - C
                                                   27.8
                                                               (
                                               NR
   CONSTRUCTION MATERIAL GENERIC TYPE
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               NR
```

HOOSIER ENERGY: MEROM 1 (CONT.)

DEVICE TYPE

**	FANS NUMBER NUMBER OF SPARES DESIGN SUPPLIER FUNCTION APPLICATION SERVICE CONSTRUCTION MATERIAL GENERIC TYPE	2 0 CENTRIFUGAL WESTINGHOUSE BOOSTER FORCED DRAFT DRY CARBON STEEL
**	FANS NUMBER NUMBER OF SPARES DESIGN SUPPLIER FUNCTION APPLICATION SERVICE CONSTRUCTION MATERIAL GENERIC TYPE	2 0 AXIAL NOVENCO UNIT FORCED DRAFT DRY CARBON STEEL
**	DAMPERS NUMBER FUNCTION GENERIC TYPE SPECIFIC TYPE MANUFACTURER MODULATION	4 SHUT-OFF GUILLOTINE NR; SEAL AIR MOSSER OPEN
**	DAMPERS NUMBER FUNCTION GENERIC TYPE SPECIFIC TYPE MANUFACTURER MODULATION	4 SHUT-OFF GUILLOTINE NR; SEAL AIR MOSSER OPEN
**	DAMPERS NUMBER FUNCTION GENERIC TYPE SPECIFIC TYPE MANUFACTURER MODULATION	1 SHUT-OFF NR NR MOSSER CLOSED
**	DAMPERS NUMBER FUNCTION GENERIC TYPE SPECIFIC TYPE MANUFACTURER MODULATION	1 SHUT-OFF NR NR MOSSER OPEN
**	DUCTHORK SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	NR NR NR NR
**	REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE DEVICE TYPE MANUFACTURER NUMBER FULL LOAD DRY FEED CAPACITY - M.TONS/HR	TOWER MILL N/A N/A JAPAN TOWER MILL CO. 2 25.4 (28 TPH)
××	REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE	LIMESTONE PRECRUSHER

N/A

N/A

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UTILITY FGD SURVEY: OCTOBER 1983 - SEPTEMBER 1984
HOOSIER ENERGY: MEROM 1 (CONT.)
    MANUFACTURER
                                                PENNSYLVANIA CRUSHER CORP.
    NUMBER
    FULL LOAD DRY FEED CAPACITY - M.TONS/HR
                                                   25.4
                                                               ( 28 TPH)
** TANKS
    SERVICE
                                                NUMBER
    PROCESS SURGE
                                                  1
    INTERMEDIATE
 ** PUMPS
                                                NUMBER
    SERVICE
    ABSORBER
                                                  12
    ABSORBER COOLING
                                                   8
    OXIDIZER FEED
                                                   2
    THICKENER OVERFLOW
                                                   2
    THICKENER UNDERFLOW
                                                   2
    SURGE-TANK
    SEED SLURRY
    LIMESTONE SLURRY FEED [LOW HEAD]
                                                   2
    LIMESTONE SLURRY FEED [HIGH HEAD]
 ** SOLIDS CONCENTRATING/DEWATERING
    DEVICE
                                                THICKENER
    NUMBER
                                                 1
    NUMBER OF SPARES
                                                Ω
    DIMENSIONS - FT
                                                140 DIA
    CAPACITY
                                                1116000 GAL
    SHELL GENERIC MATERIAL TYPE
                                               CARBON STEEL
    SHELL SPECIFIC MATERIAL TYPE
                                               AISI 1110
    LINER GENERIC MATERIAL TYPE
                                               ORGANIC
    LINER SPECIFIC MATERIAL TYPE
                                               NR
    FEED STREAM SOURCE
                                                ABSORBER BLOWDOWN & SEED CYCLONE OVERFLOW
                                               18 % SOLIDS -
    FEED STREAM CHARACTERISTICS
    OUTLET STREAM CHARACTERISTICS
                                               35% SOLIDS
    OUTLET STREAM DISPOSITION
                                                VACUUM FILTERS
    OVERFLOW STREAM DISPOSITION
                                                FGD SYSTEM
 ** SOLIDS CONCENTRATING/DEWATERING
    DEVICE
                                                VACUUM FILTER
    NUMBER
                                                 2
    NUMBER OF SPARES
                                                0
    DIMENSIONS - FT
                                                12.0 DIA X 24
                                                THICKENER
    FEED STREAM SOURCE
                                                35 % SOLIDS
    FEED STREAM CHARACTERISTICS
                                               55 % SOLIDS
    OUTLET STREAM CHARACTERISTICS
    OUTLET STREAM DISPOSITION
                                                IUCS
*** SLUDGE
 ** TREATMENT
                                                FORCED OXIDATION
    METHOD
    DEVICE
                                                PUG MILL
                                                CONVERSION SYSTEMS [POZ-O-TEC]
    PROPRIETARY PROCESS
    INLET QUALITY - %
                                                   15.0
```

13-405

FINAL

TRUCK

HOHE

30

LANDFILL

250 ACRES X 50 FT

15360880 (12560.0 ACRE-FT)

ON-SITE

** DISPOSAL

NATURE TYPE

LOCATION

SITE TREATMENT

SITE DIMENSIONS SITE CAPACITY CU.M

SITE TRANSPORTATION METHOD

SITE SERVICE LIFE - YRS

HOOSIER ENERGY: MEROM 1 (CONT.)

** WATER BALANCE WATER LOOP TYPE

CLOSED

** CHEMICALS AND CONSUMPTION

FUNCTION NAME PRINCIPAL CONSTITUENT POINT OF ADDITION

.0

SYSTEM

ABSORBENT LIMESTONE CACO3 PRECRUSHER

PERIOD			Y OPERABILITY			% REMOVAL SO2 PART.	HOURS	HOURS	HOURS	FACTO
8/82	SYSTEM						744			
	** PROE	SLEMS/SOLUT]	ONS/COMMENTS							
			THE FGD SYSTEM STARTUP PHASE FOR MARCH.							
9/82	SYSTEM						720			
10/82	SYSTEM						744			
11/82	SYSTEM	,					720			
12/82	SYSTEM						744			
1/83	SYSTEM			الار			744			
2/83	SYSTEM			J			672			
3/83	A B C D SYSTEM	53.1 53.1 53.1 53.1 53.1	56.0 54.2 43.6	54.1 56.0 54.2 43.6 52.0	51.3 53.1 51.4 41.4 49.3		744	706	367	58.6
	** PROB	BLEMS/SOLUT]	ONS/COMMENTS							
			THE FGD SYSTE	M COMPLETED	COMPLIANCE TE	STING DURING	S THE I	нтиом	F MARC	₫.
4/83	A B C D SYSTEM	100.0 100.0 100.0 100.0	.0 74.4	100.0	3.1 3.1 .0 3.1 2.3		720	30	23	35.0
	** PROB	BLEMS/SOLUT]	ONS/COMMENTS							
			THE UNIT WAS	TAKEN OUT OF	SERVICE ON A	APRIL 2 FOR S	STACK I	REPAIRS		
5/83	A B C D System	.0 .0 .0			.0 .0 .0			0	0	
6/83	A B C	.0			.0		, , , ,	Ū	Ū	

.0

720 0

0

HOOSIER ENERGY: MEROM 1 (CONT.)

7/83 A B C D SYS 8/83 A B C D	.0 .0 .0 .0 .0 .0 STEM .0	TONS/COMMENTS THE UNIT REMAI REPAIRS.	INED OUT OF S	. 0 . 0	G MAY AND) JUNE FOR	CONTIN	√UED ST	'ACK
8/83 A B C D	.0 .0 .0 .0 .0 .0		TNED OUT OF S	. 0 . 0	G MAY AND) JUNE FOR	CONTI	VUED ST	ACK
8/83 A B C D	.0 .0 .0 .0 .0 .0			.0					
8/83 A B C D	.0 .0 .0 .0 .0 .0			.0					
8/83 A B C D	.0 .0 .0								
SYS 8/83 A B C D	.0 .0			. 0					
8/83 A B C	.0			.0					
B C D	.0			.0		744	0	0	
C D				.0					
D	.0			.0					
-				.0					
SYS	.0			.0					
	STEM .0			. 0		744	0	0	
××	PROBLEMS/SOLUT	IONS/COMMENTS							
		THE UNIT WAS O	OUT OF SERVIC	E DURING JUL	OUA DIA Y	SUST FOR S	TACK L	IN E R RE	PAIRS
9/83 A	15.6	16.9	17.8	12.2					
В	45.1		59.5	40.7					
c	45.1		61.0	41.7					
D	45.1	55.6	58.4	39.9					
SYS	STEM 37.8	46.8	49.2	33.6		72 0	517	242	44.4
**	PROBLEMS/SOLUT	IONS/COMMENTS							
		THE UTILITY REPROBLEMS WERE CARDS.			-		_		–
		THE UTILITY AT		RT-UP PROBLE	MS DURING	; SEPTEMBE	R TO TH	ie PREV	'Ious
.0/83 A	99.2	93.6	100.0	93.4					
В	99.2		100.0	94.4					
С	99.2	86.1	100.0	85.8					
D	99.2		100.0	86.0					
SYS	STEM 99.2	90.1	100.0	89.9		744	742	669	75.
1/83 A	98.3	98.3	98.3	98.3					
В	98.3	98.3	98.3	98.3					
С	98.3	98.3	98.3	98.3					
D	98.3	98.3	98.3	98.3					
SYS	STEM 98.3	98.3	98.3	98.3		720	720	708	77.
	PROBLEMS/SOLUT	IONS/COMMENTS							
××		NO MAJOR FGD-F	RELATED OUTAG	SES WERE ENCO	UNTERED D	URING OCT	OBER A	ND NOVE	MBER
**									
	E7 2	5/ O	EE 0	54 A					
2/83 A	57.2 57.2	54.9 54.1	55.0 54.2	54.0 53.3					
2/83 A B	57.2	54.1	54.2	53.3					
.2/83 A									

HOOSTER ENERGY: MEROM 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

EXTREME COLD WEATHER CONDITIONS DURING DECEMBER RESULTED IN TORN EXPANSION JOINTS.

A MALFUNCTION ON THE SLUDGE STABILIZATION SYSTEM OCCURRED DURING DECEMBER RESULTING FROM EXTREME COLD WEATHER CONDITIONS.

1/84	A	75.3	63.0	63.0	63.0				
	В	100.0	68.8	68.8	68.8				
	С	100.0	66.6	66.6	66.6				
	D	100.0	66.6	66.6	66.6				
	SYSTEM	93.8	66.2	66.2	66.2	744	744	493	74.0

** PROBLEMS/SOLUTIONS/COMMENTS

A MALFUNCTION IN THE SLUDGE HANDLING SYSTEM ACCOUNTED FOR A SYSTEM OUTAGE DURING JANUARY.

COMPUTER-RELATED PROBLEMS WERE ENCOUNTERED DURING THE MONTH.

FROZEN LIMESTONE ACCOUNTED FOR ADDITIONAL DOWN TIME IN JANUARY.

ADDITIONAL PROBLEMS DUE TO FREEZING WERE ENCOUNTERED DURING THE MONTH.

2/84	A	90.2	88.4	91.9	85.6				
	В	89.9	88. 0	91.5	85 . 3				
	С	90.6	88.8	92.4	86.0				
	D	90.1	88.3	91.8	85.5				
	SYSTEM	90.2	88.4	91.9	85.6	696	674	596	70.3
3/84	A	96.7	86.8	92.8	85.0				
	В	94.3	85.8	91.7	84.0				
	С	96.7	89.3	95.5	87.5				
	ם	96.7	87.3	93.3	85.5				
	SYSTEM	96.1	87.3	93.3	85.5	744	729	636	80.0

^{**} PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE REPORTED DURING FEBRUARY AND MARCH.

4/84	A	68.2	49.3	49.9	48.8				
	В	66.9	48.0	48.6	47.5				
	С	67.6	48.7	49.3	48.2				
	D	69.6	50.7	51.3	50.2				
	SYSTEM	68.1	49.2	49.8	48.7	720	712	350	69.4

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT A PUMP FAILURE AND BUCKET ELEVATOR FAILURES LED TO PROBLEMS IN THE LIMESTONE PREPARATION SYSTEM.

5/84	SYSTEM	744
6/84	SYSTEM	720
7/84	SYSTEM	744
8/84	SYSTEM	744
9/84	SYSTEM	720

HOOSIER ENERGY: MEROM 1 (CONT.)

				DEDECOMA	JCE DATA						
_											
PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% RE	MOVAL	PER	BOILER	FGD	CAP.
						S 02	PART.	HOURS	HOURS	HOURS	FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE PERIOD OF MAY THROUGH SEPTEMBER 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COMPANY NAME PLANT NAME UNIT NUMBER CITY STATE REGULATORY CLASSIFICATION PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW NET UNIT GENERATING CAPACITY W/FGD - MW NET UNIT GENERATING CAPACITY W/FGD - MW EQUIVALENT SCRUBBED CAPACITY - MW	HOOSIER ENERGY MEROM 2 MEROM INDIANA D 43. (.100 LB/MMBTU) 516. (1.200 LB/MMBTU) ****** (****** LB/MMBTU) ****** 490 460 466 441
** UNIT DATA - BOILER AND STACK BOILER SUPPLIER BOILER TYPE BOILER SERVICE LOAD DESIGN BOILER FLUE GAS FLOW - CU.M/S BOILER FLUE GAS TEMPERATURE - C STACK HEIGHT M STACK SHELL STACK TOP DIAMETER - M	RILEY STOKER PULVERIZED COAL BASE 817.33 (1732000 ACFM) ******* (**** F) 214. (702 FT) CONCRETE 5.8 (19.0 FT)
** FUEL DATA FUEL TYPE FUEL GRADE AVERAGE HEAT CONTENT - J/G RANGE HEAT CONTENT - BTU/LB AVERAGE ASH CONTENT - % RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - % AVERAGE MOISTURE CONTENT - % AVERAGE SULFUR CONTENT - % RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - %	COAL BITUMINOUS ****** (****** BTU/LB) ******* ******* ****** 3.50 ****** .20 ******
*** PARTICLE CONTROL	•
** MECHANICAL COLLECTOR NUMBER TYPE	0 NONE
** FABRIC FILTER NUMBER TYPE	0 NONE
** ESP NUMBER NUMSER OF SPARES TYPE SUPPLIER INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE - C PARTICLE REMOVAL EFFICENCY - %	1 0 COLD SIDE BUELL DIVISION, ENVIROTECH 873.0 (1850000 ACFM) 137.8 (280 F) 99.4
** PARTICLE SCRUBBER NUMBER GENERIC TYPE SPECIFIC TYPE TRADE NAME/COMMON NAME SHELL GENERIC MATERIAL SHELL SPECIFIC MATERIAL LINER GENERIC MATERIAL LINER SPECIFIC MATERIAL GAS CONTACTING DEVICE TYPE	0 NONE N/A N/A N/A N/A N/A

HOOSIER ENERGY: MEROM 2 (CONT.)

*** FGD SYSTEM

```
** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                               THROWAWAY PRODUCT
                                               WET SCRUBBING
   SO2 REMOVAL MODE
   PROCESS TYPE
                                                LIMESTONE
   SYSTEM SUPPLIER
                                               MITSUBISHI HEAVY INDUSTRIES
   A-E FIRM
                                                UNITED ENGINEERS & CONSTRUCTORS
   DEVELOPMENT LEVEL
                                                FULL SCALE
   NEW/RETROFIT
                                               HEM
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - %
                                                   99.40
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                   90.00
   ENERGY CONSUMPTION - %
                                                    1.2
   CURRENT STATUS
   COMMERCIAL START-UP
                                                 2/82
   INITIAL START-UP
                                                12/81
   CONTRACT AWARDED
                                                 3/78
** DESIGN AND OPERATING PARAMETERS
   DESIGN COAL SULFER CONTENT - %
                                                    4.20
   DESIGN COAL HEAT CONTENT - J/G
                                                24423.0
                                                               ( 10500 BTU/LB)
   DESIGN COAL ASH CONTENT - %
                                                  16.00
** QUENCHER/PRESATURATOR
   CONSTRUCTION MATERIAL GENERIC TYPE
                                                NR
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                NR
** ABSORBER
   NUMBER
                                                 4
   NUMBER OF SPARES
                                                 0
   GENERIC TYPE
                                                PACKED TOWER
   SPECIFIC TYPE
                                                GRID PACKING
   TRADE NAME/COMMON TYPE
                                                COCURRENT
   SUPPLIER
                                                MITSUBISHI
   SHELL GENERIC MATERIAL
                                                CARBON STEEL
   SHELL SPECIFIC MATERIAL
                                                ND
   SHELL MATERIAL TRADE NAME/COMMON TYPE
                                                NR
   LINER GENERIC MATERIAL
                                                NR
   LINER SPECIFIC MATERIAL
                                                NR
   LINER MATERIAL TRADE NAME/COMMON TYPE
                                                NR
                                                FIXED GRIDS
   GAS CONTACTING DEVICE TYPE
   LIQUID RECIRCULATION RATE - LITER/S
                                                 1333.
                                                               (21160 GPM)
                                                               ( 42.3 GAL/1000 ACF)
   L/G RATIO - L/CU.M
                                                   5.7
                                                               ( 500000 ACFM)
   INLET GAS FLOW - CU. M/S
                                                  235.95
                                                               ( 280 F)
   INLET GAS TEMPERATURE - C
                                                  137.8
   SO2 REMOVAL EFFICIENCY - %
                                                   90.0
** MIST ELIMINATOR
                                                MIST ELININATOR
   PRE-MIST ELIMINATOR/MIST ELIMINATOR
   NUMBER PER SYSTEM
                                                 4
   NUMBER OF SPARES PER SYSTEM
                                                 0
   NUMBER PER MODULE
                                                 1
   GEHERIC TYPE
                                                NR
   SPECIFIC TYPE
                                                NR
   TRADE NAME/COMMON TYPE
                                                NP
   CONFIGURATION
                                                HORIZONTAL
   CONSTRUCTION MATERIAL GENERIC TYPE
                                                NR
                                                NR
   CONSTRUCTION MATERIAL SPECIFIC TYPE
** REHEATER
   NUMBER
   GENERIC TYPE
                                                INDIRECT HOT AIR
                                                ΝŔ
   SPECIFIC TYPE
   TRADE NAME/COMMON TYPE
                                                NR
                                                   27.8
                                                                    50 F)
   TEMPERATURE INCREASE - C
   CONSTRUCTION MATERIAL GENERIC TYPE
                                                ND
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                NR
```

HOOSIER ENERGY: MEROM 2 (CONT.)

**	FANS NUMBER NUMBER OF SPARES DESIGN SUPPLIER FUNCTION APPLICATION SERVICE CONSTRUCTION MATERIAL GENERIC TYPE	2 0 CENTRIFUGAL WESTINGHOUSE BOOSTER FORCED DRAFT DRY CARBON STEEL
**	FANS NUMBER NUMBER OF SPARES DESIGN SUPPLIER FUNCTION APPLICATION SERVICE CONSTRUCTION MATERIAL GENERIC TYPE	2 0 AXIAL NOVENCO UNIT FORCED DRAFT DRY CARBON STEEL
**	DAMPERS NUMBER FUNCTION GENERIC TYPE SPECIFIC TYPE MANUFACTURER MODULATION	4 SHUT-OFF GUILLOTINE NR; SEAL AIR MOSSER OPEN
**	DAMPERS NUMBER FUNCTION GENERIC TYPE SPECIFIC TYPE MANUFACTURER MODULATION	4 SHUT-OFF GUILLOTINE NR; SEAL AIR MOSSER OPEN
**	DAMPERS NUMBER FUNCTION GENERIC TYPE SPECIFIC TYPE MANUFACTURER MODULATION	1 SHUT-OFF NR NR MOSSER CLOSED
**	DAMPERS NUMBER FUNCTION GENERIC TYPE SPECIFIC TYPE MANUFACTURER MODULATION	1 SHUT-OFF NR NR MOSSER OPEN
**	DUCTWORK SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	NR NR NR
**	REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE DEVICE TYPE MANUFACTURER NUMBER FULL LOAD DRY FEED CAPACITY - M.TONS/HR	TOWER MILL N/A N/A JAPAN TOWER MILL CO. 2 25.4 (28 TPH
**	REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE DEVICE TYPE	LIMESTONE PRECRUSHER N/A N/A

```
HOOSIER ENERGY: MEROM 2 (CONT.)
                                                PENNSYLVANIA CRUSHER CORP.
    MANUFACTURER
    NUMBER
                                                   25.4
                                                               ( 28 TPH)
    FULL LOAD DRY FEED CAPACITY - M.TONS/HR
** TANKS
                                                NUMBER
    SERVICE
    _____
                                                ----
    PROCESS SURGE
                                                   1
    INTERMEDIATE
                                                   3
 ** PUMPS
    SERVICE
                                                NUMBER
    -----
                                                -----
    ABSORBER
                                                  12
    ABSORBER COOLING
                                                   8
    OXIDIZER FEED
                                                   2
    THICKENER OVERFLOW
                                                   2
    THICKENER UNDERFLOW
                                                   2
    SURGE-TANK
    SEED SLURRY
    LIMESTONE SLURRY FEED [LOW HEAD]
    LIMESTONE SLURRY FEED [HIGH HEAD]
 ** SOLIDS CONCENTRATING/DEWATERING
    DEVICE
                                                THICKENER
    NUMBER
                                                 1
    NUMBER OF SPARES
                                                0
    DIMENSIONS FT
                                                140 DIA
    CAPACITY
                                                1116000 GAL
    SHELL GENERIC MATERIAL TYPE
                                                CARBON STEEL
     SHELL SPECIFIC MATERIAL TYPE
                                               AISI 1110
     LINER GENERIC MATERIAL TYPE
                                                ORGANIC
    LINER SPECIFIC MATERIAL TYPE
                                                NR
    FEED STREAM SOURCE
                                                ABSORBER BLOWDOWN & SEED CYCLONE OVERFLOW
    FEED STREAM CHARACTERISTICS
                                                18 % SOLIDS
    OUTLET STREAM CHARACTERISTICS
                                                35% SOLIDS
    OUTLET STREAM DISPOSITION
                                                VACUUM FILTERS
    OVERFLOW STREAM DISPOSITION
                                                FGD SYSTEM
 ** SOLIDS CONCENTRATING/DEWATERING
    DEVICE
                                                VACUUM FILTER
    NUMBER
                                                2
    NUMBER OF SPARES
                                                0
    DIMENSIONS - FT
                                                12.0 DIA X 24
    FEED STREAM SOURCE
                                                THICKENER
    FEED STREAM CHARACTERISTICS
                                               35 % SOLIDS
    OUTLET STREAM CHARACTERISTICS
                                               55 % SOLIDS
    OUTLET STREAM DISPOSITION
                                                IUCS
*** SLUDGE
 ** TREATMENT
                                                FORCED OXIDATION
    METHOD
    DEVICE
                                                PUG MILL
                                                CONVERSION SYSTEMS [POZ-O-TEC]
    PROPRIETARY PROCESS
    INLET QUALITY - %
                                                  15.0
 ** DISPOSAL
    NATURE
                                                FINAL
```

LANDFILL

250 ACRES X 50 FT

15360880 (12560.0 ACRE-FT)

ON-SITE

TRUCK

HONE

30

TYPE

LOCATION

SITE TREATMENT

SITE DIMENSIONS SITE CAPACITY - CU.M

SITE TRANSPORTATION METHOD

SITE SERVICE LIFE - YRS

HOOSIER ENERGY: MEROM 2 (CONT.)

** WATER BALANCE
WATER LOOP TYPE

12/81 SYSTEM

TYPE CLOSED

** CHEMICALS AND CONSUMPTION

FUNCTION
NAME
PRINCIPAL CONSTITUENT
POINT OF ADDITION

ABSORBENT LIMESTONE CACO3 PRECRUSHER

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

ON DECEMBER 30, 1981 OPERATION OF THE FGD SYSTEM INSTALLED ON MEROM 2 COMMENCED. THE SYSTEM IS PRESENTLY IN THE START UP PHASE WITH COMMERCIAL OPERATION SCHEDULED FOR FEBRUARY.

744

 1/82
 SYSTEH
 744

 2/82
 SYSTEH
 672

 3/82
 SYSTEH
 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT COMMERCIAL OPERATION WAS INITIATED ON THE FIRST OF FEBRUARY. EXCEPT FOR SOME MINOR FREEZING PROBLEMS, NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE FIRST QUARTER PERIOD.

HOWEVER, THE UTILITY DID REPORT THAT HIGH FLYASH LOADINGS TO THE ABSORBER WERE ENCOUNTERED DUE TO ESP INABILITY TO REMOVE FLYASH FROM ITS HOPPERS. THE PROBLEM WAS PARTIALLY DUE TO THE HIGH MOISTURE CONTENT OF THE COAL (FLY ASH STICKS IN THE HOPPERS AND EVENTUALLY TRIPS ESP) IN ADDITION TO FIRING WITH OIL DURING STARTUP (FLYASH STICKS TO OIL RESIDUE LEFT ON PLATES).

4/82	SYSTEM	19.8	720
5/82	SYSTEM	48.3	744
6/82	SYSTEM	30.0	720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED EXPERIENCING PROBLEMS WITH THE LINER CRACKING IN THE THICKENERS AND SETTLING IN THE SURGE TANKS DOWNSTREAM OF THE THICKENERS. FGD AVAILABILITY FOR THE FIRST SIX MONTHS OF OPERATION WAS APPROXIMATELY 25 PERCENT.

	SYSTEM	80.5	77.3	77.3	66.4	744	640	494	48.7
	D	80.5	77.3	77.3	66.4				
	С	80.5	77.3	77.3	66.4				
	В	80.5	77.3	77.3	66.4				
7/82	A	80.5	77.3	77.3	66.4				

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM EXPERIENCED A TOTAL OUTAGE TIME OF 145.2 HOURS DURING JULY. 104.5 HOURS OF THAT PERIOD WAS DUE TO A UNIT OUTAGE.

PART OF THE FGD SYSTEM OUTAGE WAS DUE TO AN INSPECTION OF THE PROCESS TANKS.

A THICKENER LINER FAILURE ALSO CONTRIBUTED TO THE OUTAGE DURING JULY.

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

A 13 HOUR OUTAGE DURING JULY WAS THE RESULT OF AN EFFORT TO UNPLUG THE THICKENER UNDERFLOW LINES.

PROBLEMS WITH A PRECIPITATOR LED TO A 13.5 HOUR OUTAGE DURING THE MONTH.

A 74 HOUR OUTAGE OCCURRED DURING THE MONTH DUE TO EXTENDED FGD MAINTENANCE FOLLOWING THE UNIT OUTAGE.

8/82	A	55.0	54.1	54.1	53.0
	В	55.0	54.1	54.1	53.0
	С	55.0	54.1	54.1	53.0
	D	55.0	54.1	54.1	53.0
	SYSTEM	55.0	54.1	54.1	53.0

744 729 394 46.0

** PROBLEMS/SOLUTIONS/COMMENTS

A BREAKDOWN OF THE LIMESTONE PREPARATION SYSTEM LED TO A 334 HOUR OUTAGE DURING AUGUST. THE BUCKET ELEVATOR CHAINS HAD TO BE REPLACED DUE TO CRACKED LINKS IN THE CHAINS. THE UTILITY REPORTED THAT DUE TO THE NATURE OF THE FAILURE, IT APPEARED THAT THE LINKS WERE DEFECTIVE.

9/82	A	76.4	22.9	22.9	7.0				
	В	76.4	22.9	22.9	7.0				
	С	76.4	22.9	22.9	7.0				
	D	76.4	22.9	22.9	7.0				
	SYSTEM	76.4	22.9	22.9	7.0	720	221	51	46.0

^{**} PROBLEMS/SOLUTIONS/COMMENTS

A FAILURE OF THE LIMESTONE PREPARATION SYSTEM RESULTED FROM A PLUGGING PROBLEM AND CAUSED A 6.5 HOUR OUTAGE DURING SEPTEMBER.

A 163.5 HOUR OUTAGE DURING THE MONTH WAS DUE TO PLUGGED WALL WASH LINES IN THE QUENCHER SECTION. ALL LINES IN ALL FOUR MODULES WERE PLUGGED AND THE CAUSE WAS SUSPECTED OF BEING A DESIGN DEFICIENCY IN THE SYSTEM. THE LINES WERE UNPLUGGED WITHIN A MATTER OF DAYS AND THE SYSTEM WAS ALLOWED TO CONTINUE OPERATING WITHOUT THE WALL WASH.

10/82	A	87.3	49.7	52.4	49.3	
	В	87.3	57.3	60.5	56.9	
	С	87.3	65.7	69.4	65.2	
	D	87.3	76.4	80.7	75.8	
	SYSTEM	87.3	62.3	65.8	61.8	

744 738 460 47.7

** PROBLEMS/SOLUTIONS/COMMENTS

DURING OCTOBER PROBLEMS WITH A PRECIPITATOR LED TO A 39 HOUR OUTAGE.

A 21 HOUR OUTAGE OCCURRED DURING THE MONTH AS A RESULT OF A COMPUTER MALFUNCTION.

A FAILURE IN THE LIMESTONE SLURRY PREPARATION SYSTEM PRODUCED A 19.5 HOUR OUTAGE DURING OCTOBER.

DURING THE MONTH THE UNIT OPERATED TYPICALLY WITH THREE MODULES ONLY DUE TO LOW BOILER LOADS.

11/82	A	47.4	46.2	46.3	45.6				
	В	47.4	46.2	46.3	45.6				
	С	47.4	37.3	37.3	36.8				
	D	47.4	13.6	13.6	13.4				
	SYSTEM	47.4	35.8	35.9	35. 3	720	711	254	48.4

HOOSIER ENERGY: MEROM 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

DURING NOVEMBER PROBLEMS WITH A PRECIPITATOR LED TO A 13 HOUR OUTAGE.

A FAILURE IN THE LIMESTONE SLURRY PREPARATION SYSTEM PRODUCED A 51.5 HOUR OUTAGE DURING NOVEMBER.

BYPASS DAMPER PROBLEMS CREATED A BRIEF 1 HOUR OUTAGE DURING THE MONTH.

A TOTAL FAILURE OF THE EXPANSION JOINTS THROUGHOUT THE FGD SYSTEM RESULTED IN A $326.5\,$ HOUR OUTAGE DURING NOVEMBER.

THE UNIT CONTINUED OPERATING WITH THREE MODULES ONLY DURING THE MONTH DUE TO LOW LOADS.

12/82	A	.0	.0	. 0	. 0			
	В	.0	.0	.0	.0			
	С	.0	.0	.0	.0			
	ם	. 0	.0	.0	.0			
	SYSTEM	.0	.0	.0	.0	744	269	0 44.6

** PROBLEMS/SOLUTIONS/COMMENTS

THE EXPANSION JOINT FAILURE PROBLEM WITHIN THE FGD SYSTEM CONTINUED DURING DECEMBER. REPLACEMENT OF THE JOINTS WAS IN PROGRESS.

1/83	A	.0	۰.0	.0	.0				
	В	.0	.0	.0	.0				
	С	.0	.0	.0	.0				
	D	.0	.0	.0	.0				
	SYSTEM	. 0	.0	.0	.0	744	744	0	47.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE EXPANSION JOINT FAILURE PROBLEM CONTINUED DURING JANUARY AND REPLACEMENT OF THE JOINTS WAS STILL IN PROGRESS.

2/83	A	.0	.0	.0	.0			
	В	.0	.0	.0	.0			
	С	.0	.0	.0	.0			
	ם	.0	.0	.0	. 0			
	SYSTEM	. 0	.0	.0	.0	672	667	50.2

** PROBLEMS/SOLUTIONS/COMMENTS

THE EXPANSION JOINT FAILURE PROBLEM CONTINUED DURING FEBRUARY AND REPLACEMENT OF THE JOINTS WAS STILL IN PROGRESS.

3/83	A	64 .5	. 0	.0			
	В	64.5	. 0	.0			
	С	64.5	.0	. 0			
	D	64.5	. 0	.0			
	SYSTEM	64.5	.0	.0	744	40	0 44.3

** PROBLEMS/SOLUTIONS/COMMENTS

THE CONTINUATION OF EXPANSION JOINT REPAIRS OCCURRED DURING MARCH.

4/83	A B C	59.0 75.7 75.7	35.4 84.7 74.7	37.9 90.7 79.9	29.4 70.3 62.0			
	D	67.8	45.9	49.2	38.1			
	SYSTEM	69.5	60.2	64.4	49.9	720	5 97	360 57.8

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT MODIFICATIONS WERE MADE TO MODULES A AND D DURING APRIL.

COMPUTER MALFUNCTIONS WERE ATTRIBUTED TO PART OF THE 175 HOUR OUTAGES DURING THE MONTH.

PLUGGED SPRAY HEADER LINES ALSO CONTRIBUTED TO THE 175 HOUR OUTAGES IN APRI

ESP MALFUNCTIONS CONTRIBUTED TO 39 HOURS OF FGD OUTAGE IN APRIL.

5/83	A	95.8	88.6	88.6	88.6				
	В	95.8	85.0	85.0	85.0				
	С	76.4	61.2	61.2	61.2				
	D	95.8	95.5	95.5	95.5				
	SYSTEM	90.9	82.6	82.6	82.6	744	744	614	60.3

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING MAY.

6/83	A	21.9	86.9	86.9	21.9				
	В	1.3	5.2	5.2	1.3				
	С	21.9	82.0	82.0	20.7				
	D	21.9	86.2	86.2	21.7				
	SYSTEM	16.8	65.1	65.1	16.4	720	182	118	53.6

** PROBLEMS/SOLUTIONS/COMMENTS

EXTENSIVE SCHEDULED MAINTENANCE WAS PERFORMED ON THE FGD SYSTEM DURING A BOILER OUTAGE IN JUNE.

7/83	A	100.0	73.2	72.9	72.6			
	В	100.0	99.9	99.5	99.1			
	С	100.0	100.0	100.0	99.6			
	D	100.0	61.0	60.7	60.5			
	SYSTEM	100.0	83.5	83.3	82.9	744	738	617 71.5

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS PARTIALLY BYPASSED DURING JULY TO MINIMIZE STACK LINER CRACKING BY MAINTAINING A SPECIFIC TEMPERATURE RANGE WITHIN THE STACK. THE UTILITY ATTRIBUTED LOWER SO2 REMOVAL EFFICIENCIES TO THE BYPASS INCIDENT.

LINER REPAIRS ARE SCHEDULED FOR THE FALL OF 1983.

THE UNIT EXPERIENCED AN AIR HEATER FAILURE DURING JULY AND THE FGD SYSTEM WAS CONSEQUENTLY USED TO COOL GAS, PROTECTING THE STACK LINER.

8/83	A	99.7	98.8	99.5	85.8				
	В	99.7	98. 9	99.6	85.9				
	С	99.7	99.2	100.0	86.2				
	D	99.7	97.9	98.6	85.0				
	SYSTEM	99.7	98.7	99.4	85.7	744	646	638	65.4

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS AGAIN PARTIALLY BYPASSED DURING AUGUST TO MINIMIZE STACK LINER CRACKING BY MAINTAINING A SPECIFIC TEMPERATURE WITHIN THE STACK.

9/83 A 97.2 88.3 90.4 38.1

HOOSIER ENERGY: MEROM 2 (CONT.)

DEDION	MODIN F	AVATLARTLITY	OPERABILITY	PERFORMA	NCE DATA UTILIZATION	 % RE	MOVAL	PER	BOILER	FGD	CAP.
PERIOD	HODOLL					502	PART.	HOURS	HOURS	HOURS	FACTOR
	В	97.9	90.0	92.2	38.9						
	С	97.9	90. 0	92.2	38.9						
	D	98.6	90.0	92.2					•••		
	SYSTEM	97.9	89.6	91.7	38.7			720	311	278	28.6
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
		Т	HE FALL SCHE	DULED OUTAGE	FOR STACK LI	NER R	EPAIRS	COMME	NCED IN	SEPTE	MBER.
10/83		100.0			.0						
	В	100.0			.0						
	C	100.0 100.0			.0						
	D SYSTEM				. 0			744	0	0	
11/83	A	100.0			. 0						
	В	100.0			.0						
	С	100.0			.0						
	D	100.0			.0						
	SYSTEM	100.0			.0			720	0	0	.0
12/83											
	В										
	C										
	D System							744	0		
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			HE UTILITY R		THE UNIT WAS	S OUT	OF SER	VICE D	URING T	HE FOU	RTH
			OARTER OF 17	03.	_						
1/84	A	.0			.0						
	В	.0			.0						
	С	.0			.0						
	D	. 0			.0			744	. 0	0	.0
	SYSTEM	.0			. 0			744	. 0	U	.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
		ד	THE UNIT WAS	OUT OF SERVI	CE THROUGHOUT	JANU	JARY.				
2/84	A	.0	.0		.0						
	В	.0	.0		.0						
	С	.0	.0		.0						
	D	.0	.0		.0						
	SYSTEM	.0	.0		.0			6 96	54	C	2.6
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
					T STACKLINER I			OMPLET	CMA DE	THE UN	IT.
3 /84	A	.0	.0		. 0						
	В	. 0	. 0		.0						
	С	. 0	.0		.0						
	D	.0	.0		.0						
	SYSTEM	1 .0	.0		.0			744	66	()
	** PRO	BLEMS/SOLUTIO	DNS/COMMENTS								

THE UNIT WAS SHUT DOWN ON MARCH 3 FOR TURBINE REPAIRS. THE REPAIRS WERE

COMPLETED ON MARCH 31.

HOOSIER ENERGY: MEROM 2 (CONT.)

				PERFORMAI	NCE DATA						
		AVAILABILITY				% RE	10VAL	PER	BOILER HOURS	FGD	CAP.
4/84	A	82.3	74.5	74.9	74.1						
	В	81.8	74.1	74.5	73.7						
	С	83.0	75.2	75.6	74.9						
	D	75.1	67.3	67.6	67.0						
	SYSTEM	80.5	72.8	73.1	72.4			720	717	522	77.6

** PROBLEMS/SOLUTIONS/COMMENTS

A BUCKET ELEVATOR FAILURE LED TO PROBLEMS IN THE LIMESTONE PREPARATION SYSTEM.

5/84	SYSTEM	744
6/84	SYSTEM	720
7/84	SYSTEM	744
8/84	SYSTEM	744
9/84	SYSTEM	720

^{**} PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE PERIOD OF MAY THROUGH SEPTEMBER 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

______ HOUSTON LIGHTING & POWER COMPANY NAME W.A. PARISH PLANT NAME A UNIT NUMBER THOMPSONS CITY TFYAS STATE REGULATORY CLASSIFICATION В PARTICULATE EMISSION LIMITATION - NG/J 13. (.030 LB/MMBTU) 155. (.360 LB/MMBTU) 215. (.500 LB/MMBTU) SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J 3670 NET PLANT GENERATING CAPACITY - MW NET PLANT GENERATING CAPACITY - MW
GROSS UNIT GENERATING CAPACITY - MW
NET UNIT GENERATING CAPACITY W/FGD - MW
NET UNIT GENERATING CAPACITY WO/FGD - MW 600 545 551 EQUIVALENT SCRUBBED CAPACITY MW 492 ** UNIT DATA - BOILER AND STACK COMBUSTION ENGINEERING BOILER SUPPLIER PULVERIZED COAL BOILER TYPE BOILER SERVICE LOAD

DESIGN EOILER FLUE GAS FLOW - CU.M/S

BOILER FLUE GAS TEMPERATURE - C

STACK HEIGHT - M

STACK SHELL

CONCRETE BOILER SERVICE LOAD BASE STACK TOP DIAMETER - M 6.7 (22.0 FT) ** FUEL DATA FUEL TYPE COAL FUEL GRADE SUBBITUMIÑOUS AVERAGE HEAT CONTENT - J/G 20799. (8942 BTU/LB) RANGE HEAT CONTENT - BTU/LB 4.75 8000-8785/8800-9636 AVERAGE ASH CONTENT - % 4.75 4.77-10.00/2.26-6.00 RANGE ASH CONTENT % AVERAGE MOISTURE CONTENT - % AVERAGE MOISTURE CONTENT - % 26.69

RANGE MOISTURE CONTENT - % 25.98-31.30/21.17-27.67

AVERAGE SULFUR CONTENT - % .41

RANGE SULFUR CONTENT - % .34-.79/.08-.60

AVERAGE CHLORIDE CONTENT - % .01 26.69 AVERAGE CHLORIDE CONTENT - % .01 RANGE CHLORIDE CONTENT - % .01 *** PARTICLE CONTROL ** FABRIC FILTER NUMBER TYPE REVERSE FLOW SUPPLIER. RESEARCH-COTTRELL 40 NUMBER OF COMPARTMENTS NUMBER OF SPARE COMPARTMENTS NUMBER OF SPARE COMPARTMENTS

INLET FLUE GAS CAPACITY - CU.M/S

INLET FLUE GAS TEMPERATURE - C

PRESSURE DROP - KPA

PARTICLE REMOVAL EFFICENCY - %

1.9

99.8 4 TYPICAL GAS/CLOTH RATIO - M/MIN (1.9 FT/MIN) .6 ** PARTICLE SCRUBBER NUMBER n GENERIC TYPE HONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL N/A LINER GENERIC MATERIAL N/A LINER SPECIFIC MATERIAL N/A GAS CONTACTING DEVICE TYPE N/A *** FGD SYSTEM ** GENERAL DATA SALEABLE FRODUCT/THROWAWAY PRODUCT THROWAWAY PRODUCT

WET SCRUBBING

SO2 REMOVAL MODE

HOUSTON LIGHTING & POWER: W.A. PARISH 8 (CONT.)

```
PROCESS TYPE
                                                   LIMESTONE
   PROCESS ADDITIVES
                                                   NONE
                                                    GE ENVIRONMENTAL SERVICES
   SYSTEM SUPPLIER
   A-E FIRM
                                                    BECHTEL
   DEVELOPMENT LEVEL
                                                    FULL SCALE
   NEW/RETROFIT
                                                   NEW
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.80
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                     70.00
   ENERGY CONSUMPTION - %
   CURRENT STATUS
   COMMERCIAL START-UP
                                                   12/82
   INITIAL START-UP
                                                   10/82
   CONTRACT AWARDED
                                                    8/79
** DESIGN AND OPERATING PARAMETERS
   DESIGN COAL SULFER CONTENT - %
   DESIGN COAL HEAT CONTENT - J/G
DESIGN COAL ASH CONTENT - %
                                                   20510.7
                                                                   ( 8818 BTU/LB)
                                                    6.13
   DESIGN MOISTURE CONTENT - X
                                                       26.24
   DESIGN CHLORIDE CONTENT - X
                                                         .02
    SPACE REQUIREMENTS - SQ M
                                                    9673.2
                                                                    ( 104125 SQ FT)
** QUENCHER/PRESATURATOR
   AISI 1110; HYDRAULICALLY-BONDED MORTAR
** ABSORBER
   NUMBER
                                                    3
   NUMBER OF SPARES
                                                    1
    GENERIC TYPE
                                                    SPRAY TOWER
   SPECIFIC TYPE
                                                   OPEN COUNTERCURRENT SPRAY
    TRADE NAME/COMMON TYPE
                                                   N/A
   SUPPLIER
                                                   GE ENVIRONMENTAL SERVICES
   DIMENSIONS - FT
                                                   40.0 DIA X 90.3
   SHELL GENERIC MATERIAL
                                                   STAINLESS STEEL
    SHELL SPECIFIC MATERIAL
                                                   AUSTENITIC
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                                  TYPE 316L
    LINER GENERIC MATERIAL
                                                    ORGANIC
    LINER SPECIFIC MATERIAL
                                                   FIBERGLASS REINFORCED
    LINER MATERIAL TRADE NAME/COMMON TYPE CEILCOTE 2500AR GAS CONTACTING DEVICE TYPE NONE
    GAS CONTACTING DEVICE TYPE
   NUMBER OF CONTACTING ZONES
                                                    3
   DISTANCE BETHEEN GAS CONTACTING ZONES - CM 152.4 ( 60.0IN)
LIQUID RECIRCULATION RATE - LITER/S 2142. (34000 GPM)
L/G RATIO - L/CU.M 5.6 ( 42.0 GAL/1000 ACF)
GAS-SIDE PRESSURE DROP - KPA .7 ( 2.7 IN-H20)
SUPERFICAL GAS VELOCITY - M/SEC 3.0 ( 9.9 FT/S)
INLET GAS TEMPERATURE - C 148.9 ( 300 F)
SO2 PEMOVAL FEETCLENCY - 2
    SO2 REMOVAL EFFICIENCY - %
                                                       85.0
** MIST ELIMINATOR
   PRE-MIST ELIMINATOR/MIST ELIMINATOR PRIMARY COLLECTOR
   NUMBER PER SYSTEM
                                                    3
   NUMBER OF SPARES PER SYSTEM
                                                     G
   NUMBER PER MODULE
                                                    1
                                                   IMPINGEMENT
   GENERIC TYPE
   SPECIFIC TYPE
                                                   BAFFLE
   TRADE NAME/COMMON TYPE
                                                   CLOSED VANE
   MANUFACTURER
                                                   GE ENVIRONMENTAL SERVICES
   CONFIGURATION
                                                   HORIZONTAL
   NUMBER OF STAGES
                                                       1
   NUMBER OF PASSES PER STAGE
                                                        4
                                                   3.66
.51
7.6
56
                                                       3.66 (12.0 FT)
.51 ( .2 IN)
   FREEBOARD DISTANCE M
   DISTANCE BETWEEN STAGES CM
                                                       7.6
                                                                  ( 3.00 IN)
   DISTANCE BETWEEN VANES - CM
   VANE ANGLES DEGREES
PRESSURE DROP KPA
                                                    .1
                                                                    ( .3 IN-H20)
                                                        3.0 ( 9.9 FT/S)
   SUPERFICAL GAS VELOCITY - M/S
   SUPERFICAL GAS VELOCITY - M/S 3.0
CONSTRUCTION MATERIAL GENERIC TYPE ORGANIC
CONSTRUCTION MATERIAL SPECIFIC TYPE POLYPROPYLENE
```

HOUSTON LIGHTING & POWER: W.A. PARISH 8 (CONT.)

```
FRESH
    WASH WATER SOURCE
                                                             ( 200 GAL/MIN)
                                                 12.6
   WASH RATE - L/S
** REHEATER
                                                a
   NUMBER
                                               BYPASS
    GENERIC TYPE
                                               COLD SIDE
    SPECIFIC TYPE
    TRADE NAME/COMMON TYPE
                                               N/A
    PERCENT GAS BYPASSED - AVG
                                                 18.0
                                                             ( 32 F)
                                                 17.8
    TEMPERATURE INCREASE - C
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               NR
                                               NR
    CONSTRUCTION MATERIAL SPECIFIC TYPE
** FANS
                                                4
    NUMBER
    NUMBER OF SPARES
                                                n
                                               CENTRIFUGAL
    DESTON
                                               GREEN FAN
    SUPPLIER
                                               UNIT
    FUNCTION
                                               FORCED DRAFT
    APPLICATION
    SERVICE
                                               DRY
                                                259.54
    FLUE GAS FLOW RATE - CU.M/S
                                                             ( 550000 ACFM)
    FLUE GAS TEMPERATURE - C
                                                148.9
                                                             ( 300 F)
                                                              (44.0 IN-H20)
    PRESSURE DROP - KPA
                                                 13.4
    CONSTRUCTION MATERIAL GENERIC TYPE
                                              CARBON STEEL
** DAMPERS
   NUMBER
                                                1
                                               CONTROL
    FUNCTION
                                               LOUVER
    GENERIC TYPE
    SPECIFIC TYPE
                                               OPPOSED BLADE
    MANUFACTURER
                                               ANDCO
    MODULATION
                                               NR
    SEAL AIR FLOW - CU. M/S
                                                   1.51
                                                             ( 3200 ACFM)
    SERVICE CONDITIONS
                                               300
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL
                                               CORTEN
    CONSTRUCTION MATERIAL SPECIFIC TYPE
    LINER GENERIC MATERIAL TYPE
                                               NP
    LINER SPECIFIC MATERIAL TYPE
                                               NR
** DAMPERS
   NUMBER
                                                1
    FUNCTION
                                               SHUT-OFF
    GENERIC TYPE
                                               GUILLOTINE
    SPECIFIC TYPE
                                               SINGLE BLADE
    MANUFACTURER
                                               ANDCO
    MODULATION
                                               NR
    SEAL AIR FLOW - CU. M/S
                                                   1.51
                                                             (
                                                                3200 ACFM)
    SERVICE CONDITIONS
                                               300
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               CORTEN
    LINER GENERIC MATERIAL TYPE
                                               NR
    LINER SPECIFIC MATERIAL TYPE
                                               ΝP
** DAMPERS
   NUMBER
    FUNCTION
                                               SHUT-OFF
    GENERIC TYPE
                                               GUILLOTINE
    SPECIFIC TYPE
                                               SINGLE BLADE
    MANUFACTURER
                                               ANDCO
    MODULATION
                                               NR
    SEAL AIR FLOW - CU. M/S
                                                          ( 3200 ACFM)
                                                   1.51
    SERVICE CONDITIONS
                                               300
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               STAINLESS STEEL
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               317L
    LINER GENERIC MATERIAL TYPE
                                               NR
    LINER SPECIFIC MATERIAL TYPE
                                               NR
** DUCTWORK
    LOCATION
                                               UPSTREAM
    CONFIGURATION
                                               RECTANGULAR
```

STON LIGHTING & POWER: W A PARISH & (CONT.)

HOUSTON LIGHTING & POWER: W.A. PARISH 8 (CONT.)	
DIMENSIONS SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	22X15.6 CARBON STEEL ASTM A-36 NONE NONE
** DUCTWORK LOCATION CONFIGURATION DIMENSIONS SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	DOWNSTREAM RECTANGULAR 16.1X16.1 CARBON STEEL ASTM A-36 INORGANIC HYDRAULICALLY-BONDED MORTAR
** REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE DEVICE TYPE MANUFACTURER NUMBER NUMBER NUMBER OF SPARES FULL LOAD DRY FEED CAPACITY - M.TONS/HR PRODUCT QUALITY - % SOLIDS	WET BALL MILL COMPARTMENTED NR K.V.S. 2 1 3.6 (4 TPH) 40.0
** TANKS SERVICE REAGENT PREP PRODUCT THICKENER OVERFLOW THICKENER UNDERFLOW THICKENER	NUMBER 1 1 1 1
** PUMPS SERVICE LIMESTONE SLURRY OVERFLOW THICKENER UNDERFLOW ABSORBER BLEED THICKENER TUNNEL SUMP LIMESTONE AREA SUMP ABSORBER RECIRCULATION	NUMBER 1 2 2 2 2 2 2 9
** SOLIDS CONCENTRATING/DEWATERING DEVICE NUMBER NUMBER OF SPARES CONFIGURATION DIMENSIONS - FT CAPACITY SHELL GENERIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE BELT GENERIC MATERIAL TYPE BELT GENERIC MATERIAL TYPE FEED STREAM SOURCE FEED STREAM CHARACTERISTICS OUTLET STREAM CHARACTERISTICS OVERFLOW STREAM DISPOSITION	VACUUM FILTER 2 0 PARALLEL 12X20 63 TON/HOUR CARBON STEEL ORGANIC NATURAL RUBBER CLOTH THICKENER UNDERFLOW 600 GPM, 25% SOLIDS 60% SOLIDS 400 GPM, 0% SOLIDS MAKEUP
** SOLIDS CONCENTRATING/DEWATERING DEVICE NUMBER NUMBER OF SPARES CONFIGURATION DIMENSIONS - FT CAFACITY SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE	THICKENER 1 0 ROUND 60.0 DIA X 15.0 416300 CARBON STEEL ASTM A-283 ASPHALTIC MEMBRANE

HOUSTON LIGHTING & POWER: W.A. PARISH 8 (CONT.)

LINER SPECIFIC MATERIAL TYPE FEED STREAM SOURCE FEED STREAM CHARACTERISTICS OUTLET STREAM CHARACTERISTICS OVERFLOW STREAM CHARACTERISTICS OUTLET STREAM DISPOSITION OVERFLOW STREAM DISPOSITION

FABRIC REINFORCED ABSORBER BLEED 328 GPM, 7% SOLIDS 66 GPM, 30% SOLIDS 298 GPM, 2.5% SOLIDS FILTRATION MAKEUP

*** SLUDGE

FULL LOAD SLUDGE QUANTITY - M.TONS/HR (DRY) 39.9 (44.0 TPH) MOISTURE CONTENT - % TOTAL FREE WATER 70.0

** TREATMENT

METHOD DEVICE PROPRIETARY PROCESS INLET QUALITY - %

STABILIZATION PUG MILL RESEARCH-COTTRELL 60.0

** DISPOSAL

NATURE TYPE LOCATION SITE TRANSPORTATION METHOD SITE TREATMENT SITE DIMENSIONS SITE SERVICE LIFE - YRS

FINAL LANDFILL ON-SITE TRUCK CLAY LINING 25 ACRES 3

** PROCESS CONTROL AND INSTRUMENTATION

CHEMICAL PARAMETERS PHYSICAL VARIABLES PROCESS CONTROL MANNER PROCESS CHEMISTRY MODE

PH FLOW, DENSITY AUTOMATIC FEED FORWARD

** WATER BALANCE

WATER LOOP TYPE

CLOSED

** CHEMICALS AND CONSUMPTION FUNCTION

NAME FRINCIPAL CONSTITUENT CONSUMPTION POINT OF ADDITION

ABSORBENT LIMESTONE CALCIUM 130 TON/DAY BALL MILL

** FGD SPARE CAPACITY INDICES

ABSORBER - %	50.0
MIST ELIMINATOR - %	.0
FAN %	50.0
BALL MILL - %	100.0
RECIRCULATION PUMP - %	50.0
THICKENER - %	.0
VACUUM FILTER - %	.0

** FGD SPARE COMPONENT INDICES

100 SPARE COMPONENT INDICES	
ABSORBER	1.0
MIST ELIMINATOR	.0
FAN	.0
BALL MILL	1.0
RECIRCULATION PUMP	1.0
THICKENER	.0
VACUUM FILTER	.0

HOUSTON LIGHTING & POWER: W.A. PARISH 8 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION X REMOVAL SO2 PART. HOURS HOURS HOURS HOURS FACTOR CAP. FACTOR 10/82 SYSTEM 744 TO THE OF THE FOD SYSTEM OCCURRED TO THE UTILITY REPORTED THAT INITIAL START-UP OF THE FOD SYSTEM OCCURRED TO THE UTILITY REPORTED THAT INITIAL START-UP OF THE FOD SYSTEM OCCURRED TO THE UTILITY REPORTED THAT INITIAL START-UP OF THE FOD SYSTEM OCCURRED TO THE UTILITY REPORTED THAT INITIAL START-UP OF THE FOD SYSTEM OCCURRED TO THE UTILITY REPORTED THAT INITIAL START-UP OF THE FOD SYSTEM OCCURRED TO THE UTILITY REPORTED THAT INITIAL START-UP OF THE FOD SYSTEM OCCURRED TO THE UTILITY REPORTED THAT NO MAJOR FOD-RELATED PROBLEMS WERE ENCOUNTERED TO THE UTILITY REPORTED THAT NO MAJOR FOD-RELATED PROBLEMS WERE ENCOUNTERED TO THE UTILITY REPORTED THAT NO MAJOR FOD-RELATED PROBLEMS WERE ENCOUNTERED TO THE UTILITY REPORTED THAT NO MAJOR FOD-RELATED PROBLEMS WERE ENCOUNTERED TO THE UTILITY REPORTED THAT NO MAJOR FOD-RELATED PROBLEMS WERE ENCOUNTERED TO THE UTILITY REPORTED THAT NO MAJOR FOD-RELATED PROBLEMS WERE ENCOUNTERED TO THE UTILITY REPORTED THAT NO MAJOR FOD-RELATED PROBLEMS WERE ENCOUNTERED TO THE UTILITY REPORTED THAT NO MAJOR FOD-RELATED PROBLEMS WERE ENCOUNTERED TO THE UTILITY REPORTED THAT NO MAJOR FOD-RELATED PROBLEMS WERE ENCOUNTERED TO THE UTILITY REPORTED THAT NO MAJOR FOD-RELATED PROBLEMS WERE ENCOUNTERED TO THE UTILITY REPORTED THAT NO MAJOR FOD-RELATED PROBLEMS WERE ENCOUNTERED TO THE UTILITY REPORTED THAT NO MAJOR FOD-RELATED PROBLEMS WERE ENCOUNTERED TO THE UTILITY REPORTED THAT NO MAJ
** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT INITIAL START-UP OF THE FGD SYSTEM OCCURRED DURING OCTOBER, 1982. 11/82 SYSTEM 720 12/82 SYSTEM 744 2/83 SYSTEM 672 3/83 SYSTEM 672 3/83 SYSTEM 744 *** PROBLEMS/SOLUTIONS/COMMENTS THE UNIT IS PRESENTLY IN THE SHAKEDOWN/DEBUGGING PHASE OF OPERATION. 4/83 SYSTEM 720 5/83 SYSTEM 744 6/83 SYSTEM 720 *** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE SECOND QUARTER OF 1983. 7/83 SYSTEM 744 8/83 SYSTEM 744
** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT INITIAL START-UP OF THE FGD SYSTEM OCCURRED DURING OCTOBER, 1982. 11/82 SYSTEM 720 12/82 SYSTEM 744 2/83 SYSTEM 672 3/83 SYSTEM 672 3/83 SYSTEM 744 *** PROBLEMS/SOLUTIONS/COMMENTS THE UNIT IS PRESENTLY IN THE SHAKEDOWN/DEBUGGING PHASE OF OPERATION. 4/83 SYSTEM 720 5/83 SYSTEM 744 6/83 SYSTEM 720 *** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE SECOND QUARTER OF 1983. 7/83 SYSTEM 744 8/83 SYSTEM 744
PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT INITIAL START-UP OF THE FGD SYSTEM OCCURRED OURING OCTOBER, 1982. THE UTILITY REPORTED THAT INITIAL START-UP OF THE FGD SYSTEM OCCURRED OURING OCTOBER, 1982. 720 744 744 744 744 744 744 748 757 768 758 758 758 758 758 758 758 758 758 75
11/82 SYSTEM 720 12/82 SYSTEM 744 1/83 SYSTEM 744 2/83 SYSTEM 672 3/83 SYSTEM 744 ** PROBLEMS/SOLUTIONS/COMMENTS
12/82 SYSTEM 744 1/83 SYSTEM 744 2/83 SYSTEM 672 3/83 SYSTEM 744 ** PROBLEMS/SOLUTIONS/COMMENTS THE UNIT IS PRESENTLY IN THE SHAKEDOWN/DEBUGGING PHASE OF OPERATION. 4/83 SYSTEM 720 5/83 SYSTEM 744 6/83 SYSTEM 720 ** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE SECOND QUARTER OF 1983. 7/83 SYSTEM 744 8/83 SYSTEM 744 9/83 SYSTEM 744 9/83 SYSTEM 744 ** PROBLEMS/SOLUTIONS/COMMENTS
1/83 SYSTEM 744 2/83 SYSTEM 672 3/83 SYSTEM 744 *** PROBLEMS/SOLUTIONS/COMMENTS THE UNIT IS PRESENTLY IN THE SHAKEDOWN/DEBUGGING PHASE OF OPERATION. 4/83 SYSTEM 720 5/83 SYSTEM 744 6/83 SYSTEM 720 *** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE SECOND QUARTER OF 1983. 7/83 SYSTEM 744 8/83 SYSTEM 744 9/83 SYSTEM 744 9/83 SYSTEM 720 *** PROBLEMS/SOLUTIONS/COMMENTS
2/83 SYSTEM 672 3/83 SYSTEM 744 *** PROBLEMS/SOLUTIONS/COMMENTS THE UNIT IS PRESENTLY IN THE SHAKEDOWN/DEBUGGING PHASE OF OPERATION. 4/83 SYSTEM 720 5/83 SYSTEM 744 6/83 SYSTEM 720 *** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE SECOND QUARTER OF 1983. 7/83 SYSTEM 744 8/83 SYSTEM 744 9/83 SYSTEM 744 9/83 SYSTEM 720 *** PROBLEMS/SOLUTIONS/COMMENTS
3/83 SYSTEM 744 ** PROBLEMS/SOLUTIONS/COMMENTS THE UNIT IS PRESENTLY IN THE SHAKEDOWN/DEBUGGING PHASE OF OPERATION. 4/83 SYSTEM 720 5/83 SYSTEM 744 6/83 SYSTEM 720 ** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE SECOND QUARTER OF 1983. 7/83 SYSTEM 744 8/83 SYSTEM 744 9/83 SYSTEM 744 9/83 SYSTEM 720 ** PROBLEMS/SOLUTIONS/COMMENTS
*** PROBLEMS/SOLUTIONS/COMMENTS THE UNIT IS PRESENTLY IN THE SHAKEDOWN/DEBUGGING PHASE OF OPERATION. 4/83 SYSTEM 720 5/83 SYSTEM 744 6/83 SYSTEM 720 *** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE SECOND QUARTER OF 1983. 7/83 SYSTEM 744 8/83 SYSTEM 744 9/83 SYSTEM 720 *** PROBLEMS/SOLUTIONS/COMMENTS
THE UNIT IS PRESENTLY IN THE SHAKEDOWN/DEBUGGING PHASE OF OPERATION. 4/83 SYSTEM 720 5/83 SYSTEM 744 6/83 SYSTEM 720 ** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE SECOND QUARTER OF 1983. 7/83 SYSTEM 744 8/83 SYSTEM 744 9/83 SYSTEM 744 ** PROBLEMS/SOLUTIONS/COMMENTS
4/83 SYSTEM 720 5/83 SYSTEM 744 6/83 SYSTEM 720 *** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE SECOND QUARTER OF 1983. 7/83 SYSTEM 744 8/83 SYSTEM 744 9/83 SYSTEM 720 *** PROBLEMS/SOLUTIONS/COMMENTS
5/83 SYSTEM 744 6/83 SYSTEM 720 *** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE SECOND QUARTER OF 1983. 7/83 SYSTEM 744 8/83 SYSTEM 744 9/83 SYSTEM 720 *** PROBLEMS/SOLUTIONS/COMMENTS
6/83 SYSTEM 720 *** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE SECOND QUARTER OF 1983. 7/83 SYSTEM 744 8/83 SYSTEM 744 9/83 SYSTEM 720 *** PROBLEMS/SOLUTIONS/COMMENTS
** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE SECOND QUARTER OF 1983. 7/83 SYSTEM 7/44 8/83 SYSTEM 7/44 9/83 SYSTEM 7/20 ** PROBLEMS/SOLUTIONS/COMMENTS
THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE SECOND QUARTER OF 1983. 7/83 SYSTEM 7/44 8/83 SYSTEM 7/83 SYSTEM 7/84 7/85 SYSTEM 7/86 PROBLEMS/SOLUTIONS/COMMENTS
DURING THE SECOND QUARTER OF 1983. 7/83 SYSTEM 744 8/83 SYSTEM 744 9/83 SYSTEM 720 ** PROBLEMS/SOLUTIONS/COMMENTS
8/83 SYSTEM 744 9/83 SYSTEM 720 ** PROBLEMS/SOLUTIONS/COMMENTS
9/83 SYSTEM 720 ** PROBLEMS/SOLUTIONS/COMMENTS
** PROBLEMS/SOLUTIONS/COMMENTS
THE SITESTLY DEPONDED THAT AND MAJOR ECD_DESATED DEORSEMS WEDE ENCOUNTEDED
DURING THE THIRD QUARTER OF 1983.
10/83 SYSTEM 744
11/83 SYSTEM 720
12/83 SYSTEM 744
** PROBLEMS/SOLUTIONS/COMMENTS
THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE FOURTH QUARTER OF 1983.
1/84 SYSTEM 744
2/84 SYSTEM 696
3/84 SYSTEM 744
4/84 SYSTEM 720
5/84 SYSTEM 744

HOUSTON LIGHTING & POWER: W.A. PARISH 8 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER SO2 PART. HOURS FACTOR

6/84 SYSTEM 720

7/84 SYSTEM 744

8/84 SYSTEM 744

9/84 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT DURING THE PERIOD OF JANUARY THROUGH SEPTEMBER 1984, EIGHT MIST ELIMINATORS WERE REPLACED. A UNIT TRIP OCCURRED CAUSING A LOSS OF AUXILIARY POWER AND A SUBSEQUENT INABILITY TO BYPASS THE FGD SYSTEM. AS A RESULT, THE EXTREME HIGH TEMPERATURE FLUE GAS ENTERED THE MIST ELIMINATORS AND BURNED THEM OUT. NO DAMAGE WAS REPORTED TO OTHER EQUIPMENT DOWSTREAM.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COMPANY NAME	INDIANAPOLIS	POWER & LIGHT
PLANT NAME	PETERSBURG	
UNIT NUMBER	3	
CITY	PETERSBURG	
- -	INDIANA	
STATE	_	
REGULATORY CLASSIFICATION	D	
PARTICULATE EMISSION LIMITATION - NG/J	43.	(.100 LB/MMBTU)
SO2 EMISSION LIMITATION - NG/J	516.	(1.200 LB/MMBTU)
NOX EMISSION LIMITATION - NG/J	301.	(1.200 LB/MMBTU) (.700 LB/MMBTU)
NET PLANT GENERATING CAPACITY - MW	1180	
GROSS UNIT GENERATING CAPACITY - MW	532	
NET UNIT GENERATING CAPACITY W/FGD - MW	515	
1121		
NET UNIT GENERATING CAPACITY WO/FGD - MW	528	
EQUIVALENT SCRUBBED CAPACITY - MW	532	
** UNIT DATA - BOILER AND STACK		
BOILER SUPPLIER	COMBUSTION EN	GINEERING
BOILER TYPE	PULVERIZED CO	
BOILER SERVICE LOAD	BASE	
DOTTER SERVICE LOAD	10/1 77	(0050000 4054)
DESIGN BOILER FLUE GAS FLOW - CU.M/S	1061.77	(2250000 ACFM)
BOILER FLUE GAS TEMPERATURE - C	137.2 188.	(279 F)
STACK HEIGHT - M	188.	(616 FT)
STACK SHELL	CONCRETE	
STACK TOP DIAMETER - M	6.1	(20.0 FT)
** FUEL DATA		
	2211	
FUEL TYPE	COAL	
FUEL GRADE	BITUMINOUS	
AVERAGE HEAT CONTENT - J/G	25004.	(10750 BTU/LB)
RANGE HEAT CONTENT - BTU/LB		10200-11000
AVERAGE ASH CONTENT - %	10.50	
RANGE ASH CONTENT - %	8-12	
AVERAGE MOISTURE CONTENT - %	10.75	
RANGE MOISTURE CONTENT - %	10.5-16.5	
AVERAGE SULFUR CONTENT - %	3.25	
RANGE SULFUR CONTENT - %	2.8-4.5	
AVERAGE CHLORIDE CONTENT - %	*****	
RANGE CHLORIDE CONTENT - %	*****	
MANGE CHECKIBE CONTENT - 7.		
YYY BIRTINI C COUTDO!		
*** PARTICLE CONTROL		
** MECHANICAL COLLECTOR		
NUMBER	0	
TYPE	NONE	
· · · · -		
** ESP		
	2	
NUMBER	-	
NUMBER OF SPARES	0	
TYPE	COLD SIDE	
SUPPLIER	RESEARCH-COTT	RELL
INLET FLUE GAS CAPACITY - CU.M/S	464.1	(983500 ACFM)
INLET FLUE GAS TEMPERATURE - C	137.2	(279 F)
PRESSURE DROP - KPA	.4	(2. IN-H2O)
	99.3	(1. 11-1120)
PARTICLE REMOVAL EFFICENCY %	99.3	
** PARTICLE SCRUBBER		
NUMBER	0	
GENERIC TYPE	NONE	
SPECIFIC TYPE	N/A	
TRADE NAME/COMMON NAME	N/A	
SHELL GENERIC MATERIAL	N/A	
SHELL SPECIFIC MATERIAL	N/A	
LINER GENERIC MATERIAL	N/A	
LINER SPECIFIC MATERIAL	N/A	
GAS CONTACTING DEVICE TYPE	N/A	
SAS CONTACTING DEVICE TIPE	17.0	

13-427

*** FGD SYSTEM

```
** GENERAL DATA
                                                    THROWAWAY PRODUCT
    SALEABLE PRODUCT/THROWAWAY PRODUCT
                                                     WET SCRUBBING
    SO2 REMOVAL MODE
                                                     LIMESTONE
    PROCESS TYPE
                                                     NONE
    PROCESS ADDITIVES
                                                     AIR CORRECTION DIVISION, UOP
    SYSTEM SUPPLIER
    A-F FTRM
                                                     GIBBS & HILL
    DEVELOPMENT LEVEL
                                                     FULL SCALE
    NEW/RETROFIT
                                                     NEW
    UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.30
UNIT DESIGN SO2 REMOVAL EFFICIENCY - % 85.00
    EMERGY CONSUMPTION - %
    CURRENT STATUS
                                                     12/77
    COMMERCIAL START-UP
    INITIAL START-UP
                                                     12/77
    CONTRACT AWARDED
                                                      1/75
** DESIGN AND OPERATING PARAMETERS
                                                       4.50
    DESIGN COAL SULFER CONTENT - %
                                                   4.50
25004.5
    DESIGN COAL HEAT CONTENT - X/G
DESIGN COAL ASH CONTENT - X
DESIGN MOISTURE CONTENT - X
DESIGN CHLORIDE CONTENT - X
                                                                     ( 10750 BTU/LB)
                                                    15.00
                                                        12.00
                                                          .06
    OPER. & MAINT, REQUIREMENT - MANHR/DAY
                                                     120 0
** QUENCHER/PRESATURATOR
    NUMBER
    TYPE
                                                     HORIZONTAL SPRAY CHAMBER
    SUPPLIER
                                                     AIR CORRECTION DIVISION, UOP
                                                     265.44 ( 562500 ACFM)
137.8 ( 280 F)
16. ( 250 GPM)
.1 ( .4 GAL/1000 ACFM)
    INLET GAS FLOW - CU. M/S
    INLET GAS TEMPERATURE - C
    LIQUID RECIRCULATION RATE - LITERS/S
    L/G RATIO - L/CU. M
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                   CARBON STEEL
                                                   AISI 1110
** ABSORBER
    NUMBER
    NUMBER OF SPARES
                                                      0
    GENERIC TYPE
                                                     PACKED TOWER
    SPECIFIC TYPE
                                                    MOBILE BED PACKING
    TRADE NAME/COMMON TYPE
                                                    TURBULENT CONTACT ABSORBER
    SUPPLIER
                                                    AIR CORRECTION DIVISION, UOP
    DIMENSIONS - FT
                                                     30.0 X 30.0 X 100.0
    SHELL GENERIC MATERIAL
                                                    CARBON STEEL
    SHELL SPECIFIC MATERIAL
                                                    AISI 1110
    SHELL MATERIAL TRADE NAME/COMMON TYPE N/A
    LINER GENERIC MATERIAL
                                                    ORGANIC
                                                    SYNTHETIC RUBBER
    LINER SPECIFIC MATERIAL
    LINER MATERIAL TRADE NAME/COMMON TYPE

NEOPRENE LS-576

GRIDS

MEDITAL TYPE

OF CONTINUE TYPE
    NUMBER OF CONTACTING ZONES

DISTANCE BETHEEN GAS CONTACTING ZONES - CM 30.5 ( 12.0IN)
LIQUID RECIRCULATION RATE - LITER/S 1386. (22000 GPM)

7 8 ( 58.7 GAL/)
                                                     7.8
2.1
4.4
                                                                    ( 58.7 GAL/1000 ACF)
    GAS-SIDE PRESSURE DROP - KPA
                                                               ( 14.5 FT/S)
( 375000 ACFM)
( 118 F)
                                                                      ( 8.5 IN-H20)
    SUPERFICAL GAS VELOCITY - M/SEC
INLET GAS FLOW - CU. M/S
INLET GAS TEMPERATURE C
                                                    4.4
176.96
                                                        47.8
    SO2 REMOVAL EFFICIENCY - %
                                                        80.0
    PARTICLE REMOVAL EFFICENCY - %
                                                       99.0
** MIST ELIMINATOR
    PRE-MIST ELIMINATOR/MIST ELIMINATOR PRIMARY COLLECTOR
    NUMBER PER SYSTEM
                                                     a
    NUMBER OF SPARES PER SYSTEM
                                                     0
    NUMBER PER MODULE
                                                     2
    GENERIC TYPE
                                                     IMPINGEMENT
    SPECIFIC TYPE
                                                    BAFFIE
    TRADE NAME/COMMON TYPE
                                                    CLOSED VANE
```

```
MANUFACTURER
                                               STRUCTURE-LITE [UOP HAS PATENT]
   CONFIGURATION
                                               HORIZONTAL
   NUMBER OF PASSES PER STAGE
                                                   3
   FREEBOARD DISTANCE - M
                                                              ( 3.0 FT)
   VANE ANGLES - DEGREES
                                                 90
   CONSTRUCTION MATERIAL GENERIC TYPE
                                               ORGANIC
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               FIBER-REINFORCED POLYESTER
   WASH WATER SOURCE
                                               THICKENER OVERFLOW, MAKEUP, TRAP-OUT TRAY RETURN
   WASH FREQUENCY
                                               CONTINUOUS
** REHEATER
                                                2
   NUMBER OF SPARES
                                                Λ
   GENERIC TYPE
                                               INDIRECT HOT AIR
   SPECIFIC TYPE
                                               EXTERNAL HEAT EXCHANGER
   TRADE NAME/COMMON TYPE
                                               STEAM TUBE BUNDLE
   LOCATION
                                               EXTERNAL
   PERCENT GAS BYPASSED - AVG
                                                    . 0
   TEMPERATURE INCREASE - C
                                                  16.7
                                                                 30 F)
   INLET FLUE GAS FLOW RATE - CU. M/S
                                                 149.59
                                                              ( 317000 ACFM)
   INLET FLUE GAS TEMPERATURE - C
                                                              ( 118 F)
                                                  47.8
   OUTLET FLUE GAS FLOW RATE - CU. M/S
                                                  74.80
                                                              ( 158500 ACFM)
   OUTLET FLUE GAS TEMPERATURE - C
                                                  64.4
                                                              ( 148 F)
   NUMBER OF HEAT EXCHANGER BANKS
                                                  1
   NUMBER OF BUNDLES PER BANK
                                                  1
   NUMBER OF TUBES PER BUNDLE
                                               565
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              CARBON STEEL
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               AISI 1110
** FANS
   NUMBER
                                                2
   NUMBER OF SPARES
                                                O
                                               CENTRIFUGAL
   DESTGN
   SUPPLIER
                                               WESTINGHOUSE
   FUNCTION
                                               BOOSTER
   APPLICATION
                                               FORCED DRAFT
   SERVICE
                                               DRY
   FLUE GAS FLOW RATE - CU.M/S
                                                224.15
                                                              ( 475000 ACFM)
   FLUE GAS TEMPERATURE - C
                                                              ( 279 F)
                                                 137.2
   CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL
** DAMPERS
   NUMBER
                                                2
                                               CONTROL
   FUNCTION
   GENERIC TYPE
                                               GUILLOTINE
   SPECIFIC TYPE
                                               SIDE-ENTRY GUILLOTINE
   MANUFACTURER
                                               ANDCO
   MODULATION
                                               OPEN/CLOSED
                                               CARBON STEEL; HIGH ALLOY [SEALS]
   CONSTRUCTION MATERIAL GENERIC TYPE
                                               AISI 1110; IRON BASE/NICKEL-CHROMIUM-COPPER-MOLY
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               NONE
   LINER GENERIC MATERIAL TYPE
   LINER SPECIFIC MATERIAL TYPE
                                               N/A
** DAMPERS
   NUMBER
                                                2
   FUNCTION
                                               SHUT-OFF
   GENERIC TYPE
                                               GUILLOTINE
   SPECIFIC TYPE
                                               NR
   MANUFACTURER
                                               ANDCO
   MODULATION
                                               OPEN/CLOSED
                                               CARBON STEEL; HIGH ALLOY [SEALS]
   CONSTRUCTION MATERIAL GENERIC TYPE
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               AISI 1110; IRON BASE/NICKEL-CHROMIUM-COPPER-MOLY
   LINER GENERIC MATERIAL TYPE
                                               NONE
   LINER SPECIFIC MATERIAL TYPE
                                               N/A
** DAMPERS
   NUMBER
   FUNCTION
                                               SHUT-OFF
   GENERIC TYPE
                                               GUILLOTINE
                                               NP
   SPECIFIC TYPE
                                               ANDCO
   MANUFACTURER
```

INDIANAPOLIS POWER & LIGHT: PETERSBURG 3 (CONT.)

MODULATION
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

OPEN/CLOSED
CARBON STEEL; HIGH ALLOY [SEALS]
AISI 1110; IRON BASE/NICKEL-CHROMIUM-COPPER-MOLY

NONE N/A

** DAMPERS

NUMBER
FUNCTION
GENERIC TYPE
SPECIFIC TYPE
MANUFACTURER
MODULATION
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

4 SHUT-OFF GUILLOTINE NR MOSSER OPEN/CLOSED

CARBON STEEL; HIGH ALLOY [SEALS]

AISI 1110; IRON BASE/NICKEL-CHROMIUM-COPPER-MOLY NONE

N/A

** DAMPERS

NUMBER
FUNCTION
GENERIC TYPE
SPECIFIC TYPE
MANUFACTURER
MODULATION
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
LINER GENERIC MATERIAL TYPE

LINER SPECIFIC MATERIAL TYPE

4 SHUT-OFF GUILLOTINE NR ANDCO

OPEN/CLOSED
CARBON STEEL; HIGH ALLOY [SEALS]

AISI 1110; IRON BASE/NICKEL-CHROMIUM-COPPER-MOLY

NONE N/A

** DAMPERS

NUMBER
FUNCTION
GENERIC TYPE
SPECIFIC TYPE
MANUFACTURER
MODULATION
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

2 SHUT-OFF GUILLOTINE NR ANDCO OPEN/CLOSED

CARBON STEEL; HIGH ALLOY [SEALS]

AISI 1110; IRON BASE/NICKEL-CHROMIUM-COPPER-MOLY

NONE N/A

** DUCTWORK

LOCATION
CONFIGURATION
DIMENSIONS
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

SCRUBBER INLET
CIRCULAR
16 FT DIA
CARBON STEEL
AISI 1110
NONE
N/A

** DUCTWORK

LOCATION
CONFIGURATION
DIMENSIONS
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

SCRUBBER OUTLET CIRCULAR 18 FT DIA CARBON STEEL AISI 1110 ORGANIC

GLASS FLAKE-FILLED POLYESTER

** DUCTWORK

LOCATION

CONFIGURATION
DIMENSIONS
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

BYPASS RECTANGULAR 16 FT X 20 FT CARBON STEEL AISI 1110 ORGANIC

GLASS FLAKE-FILLED POLYESTER

```
** REAGENT PREPARATION EQUIPMENT
                                                WET BALL MILL
    FUNCTION
    DEVICE
                                                COMPARTMENTED
    DEVICE TYPE
                                                ND
    MANUFACTURER
                                                KENNEDY VAN SAUN
    NUMBER
    NUMBER OF SPARES
                                                 0
    FULL LOAD DRY FEED CAPACITY - M.TONS/HR
                                                   38.1
                                                             ( 42 TPH)
    PRODUCT QUALITY - % SOLIDS
                                                  35.0
** TANKS
    SERVICE
                                                NUMBER
                                                ~----
    REAGENT PREP PRODUCT
    WASTE SLURRY BLEED
                                                  1
    ABSORBER RECYCLE
    THICKENER OVERFLOW
                                                  1
    SLURRY TRANSFER
    ME WASH
                                                   1
** PUMPS
    SERVICE
                                                NUMBER
                                                -----
    ABSORBER RECIRCULATION
                                                  12
    SLURRY TRANSFER
                                                   2
    WASTE SLURRY
    WASTE SLURRY BOOSTER
                                                  2
    THICKENER UNDERFLOW
    RECLAIMED WATER [THICKENER OVERFLOW]
    ME WASH
    SEAL WATER
    REHEATER CONDENSATE RETURN
 ** SOLIDS CONCENTRATING/DEWATERING
    DEVICE
                                                VACUUM FILTER
    NUMBER
                                                2
    NUMBER OF SPARES
                                                ß
    CONFIGURATION
                                               HORIZONTAL
    DIMENSIONS - FT
                                               10 DIA X 20.5
    SHELL GENERIC MATERIAL TYPE
                                               CARBON STEEL
    SHELL SPECIFIC MATERIAL TYPE
                                               AISI 1110
    LINER GENERIC MATERIAL TYPE
                                               ORGANIC
                                               COAL TAR EPOXY
    LINER SPECIFIC MATERIAL TYPE
    BELT GENERIC MATERIAL TYPE
                                                ORGANIC
    BELT SPECIFIC MATERIAL TYPE
                                               POLYPROPYLENE
    FEED STREAM SOURCE
                                               THICKENER UNDERFLOW
    FEED STREAM CHARACTERISTICS
                                               28% SOLIDS
    OUTLET STREAM CHARACTERISTICS
                                               55% SOLIDS
    OUTLET STREAM DISPOSITION
                                                SLUDGE STABILIZATION
    OVERFLOW STREAM DISPOSITION
                                                RETURNED TO SYSTEM
 ** SOLIDS CONCENTRATING/DEWATERING
    DEVICE
                                                THICKENER
    NUMBER
                                                1
    NUMBER OF SPARES
                                               n
    DIMENSIONS - FT
                                               165 DIA X 12
    CAPACITY
                                               2000000
    SHELL GENERIC MATERIAL TYPE
                                               CARBON STEEL [WALLS]; INORGANIC [BOTTOM]
    SHELL SPECIFIC MATERIAL TYPE
                                               AISI 1110; HYDRAULICALLY-BONDED CONCRETE
    LINER GENERIC MATERIAL TYPE
                                               ORGANIC
    LINER SPECIFIC MATERIAL TYPE
                                               COAL TAR EPOXY
                                               7-15% SOLIDS
    FEED STREAM CHARACTERISTICS
                                               28% SOLIDS
    OUTLET STREAM CHARACTERISTICS
                                               TO VACUUM FILTER
    OUTLET STREAM DISPOSITION
    OVERFLOW STREAM DISPOSITION
                                                TO QUENCHER, ME WASH TANK, BALL MILL, RECYCLE TA
*** SLUDGE
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(42.0 TPH)

FULL LOAD SLUDGE QUANTITY - M.TONS/HR (DRY) 38.1

UTILITY FGD SURVEY: OCTOBER 1983 - SEPTEMBER 1984
INDIANAPOLIS POWER & LIGHT: PETERSBURG 3 (CONT.)

** TREATMENT FIXATION METHOD PUG MTIL DEVICE PROPRIETARY PROCESS CONVERSION SYSTEMS [POZ-O-TEC] 60 0 INLET QUALITY - % ** DISPOSAL FINAL NATURE LANDFILL TYPE LOCATION ON-SITE TRUCK SITE TRANSPORTATION METHOD NONE SITE TREATMENT A SITE SERVICE LIFE - YRS ** PROCESS CONTROL AND INSTRUMENTATION PROCESS STREAM ABSORBER RECYCLE PH, INLET SO2, OUTLET SO AT STACK CHEMICAL PARAMETERS PHYSICAL VARIABLES FLUE GAS OUTLET FLOW PH 5.5-5.9 CONTROL LEVELS MONITOR TYPE LEEDS & NORTHRUP RECYCLE SLURRY LINE MONITOR LOCATION PROCESS CONTROL MANNER MANUAL PROCESS CHEMISTRY MODE FEEDBACK ** WATER BALANCE CLOSED WATER LOOP TYPE 55.6 (882 GPM) RIVER WATER NONE RECEIVING WATER STREAM MAKEUP WATER ADDITION - LITERS/S SOURCE OF MAKEUP WATER ** CHEMICALS AND CONSUMPTION ABSORBENT FUNCTION LIMESTONE NAME 96% CACO3, 3% MGCO3 PRINCIPAL CONSTITUENT SOURCE/SUPPLIER SOUTHERN INDIANA QUARRY CONSUMPTION 500 TPD UTILIZATION - % 83.0 POINT OF ADDITION BALL MILL ** FGD SPARE CAPACITY INDICES ABSORBER - % ٠0 MIST ELIMINATOR - % .0 REHEATER % . 0 ٠.0 FAN - % BALL MILL % . 0 VACUUM FILTER - % 50.0 ** FGD SPARE COMPONENT INDICES ABSORBER .0 MIST ELIMINATOR .0 REHEATER .0 FAN .0 BALL MILL .0 EFFLUENT HOLD TANK . 0 RECIRCULATION PUMP . 5 THICKENER .0 VACUUM FILTER .0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

12/77 SYSTEM 744

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER BEGAN COMMERCIAL OPERATIONS ON NOVEMBER 29, 1977.

OPERATION OF ALL FOUR MODULES COMMENCED DURING DECEMBER. CURRENTLY PH ADJUSTMENTS AND OTHER SHAKEDOWN PROCEDURES ARE IN PROGRESS.

REPAIRS TO THE RECYCLE TANK AGITATOR WERE REQUIRED.

COLD WEATHER ARRIVED EARLIER THAN EXPECTED. TEMPORARY ENCLOSURES WERE CONSTRUCTED AROUND SOME FGD COMPONENTS. THESE ENCLOSURES WILL BE REMOVED WHEN INSTALLATION OF HEAT TRACING CAN BE COMPLETED.

1/78 SYSTEM 744 0

** PROBLEMS/SOLUTIONS/COMMENTS

INSTALLATION OF HEAT TRACING ON FGD SYSTEM COMPONENTS WAS COMPLETED DURING THE PERIOD.

2/78 SYSTEM 672 0

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER WAS TAKEN OFF LINE ON FEBRUARY 24 TO ALLOW CORRECTION OF THE PROBLEMS ASSOCIATED WITH THE FLYASH REMOVAL SYSTEM.

PIPE AND VALVE FREEZE-UP DAMAGE WAS ENCOUNTERED AND REPAIRED.

REPAIRS WERE MADE ON THE ISOLATION DAMPERS.

3/78 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

INSULATION WAS INSTALLED ON FGD SYSTEM COMPONENTS DURING A SCHDEULED SYSTEM OUTAGE.

A BROKEN PINION GEAR IN THE THICKENER WAS REPAIRED DURING THE SYSTEM OUTAGE.

INSTRUMENTATION MAINTENANCE WAS PERFORMED DURING THE SYSTEM OUTAGE.

PROBLEMS WITH THE FLYASH HANDLING SYSTEM HAVE NOT YET BEEN SOLVED.

4/78 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS PUT BACK ON LINE IN MID-APRIL.

ALL CONTROL VALVES WERE RETURNED TO THE FACTORY FOR MODIFICATIONS. BOTH CONTROL VALVES AND PIPING HAVE BEEN PROBLEM AREAS FOR THIS SYSTEM.

5/78 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE MAIN POWER TRANSFORMER FAULTED CAUSING THE SYSTEM TO SHUTDOWN.

6/78 SYSTEM 720

INDIANAPOLIS POWER & LIGHT: PETERSBURG 3 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE SYSTEM SHUTDOWN RESULTING FROM THE MAIN POWER TRANSFORMER FAILURE IN MAY, LASTED THROUGH JUNE 16.

7/78 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM IS STILL EXPERIENCING SHAKEDOWN PROBLEMS. DURING THIS PERIOD SOME DESIGN CHANGES HAVE BEEN MADE TO IMPROVE OPERATIONS.

VALVE PROBLEMS WERE ENCOUNTERED DURING JULY. MANY VALVES HAD TO BE REMOVED AND REPAIRED.

8/78 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

PROBLEMS HAVE BEEN EXPERIENCED WITH INSTRUMENTATION.

CRACKING PROBLEMS HAVE BEEN EXPERIENCED WITH FIBERGLASS PIPING. THE PROBLEM WAS SOLVED BY REPLACING SECTIONS WITH RUBBER LINED STEEL PIPING, NEW FRP PIPING, AND PROVIDING ADDITIONAL PIPE SUPPORTS.

9/78 SYSTEM 720

10/78 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

BYPASS DAMPER PROBLEMS WERE EXPERIENCED.

AN SO2 COMPLIANCE TEST WAS INVALID DUE TO BYPASS DAMPER PROBLEMS.

11/78 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

FREEZE-UPS IN THE LIME DELIVERY SYSTEM WERE EXPERIENCED.

AN INSTRUMENTATION POWER TRANSFORMER FAILURE FORCED THE SYSTEM OUT OF SERVICE FOR ABOUT SIX DAYS.

12/78 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

MONTHLY OPERATIONAL HOURS ARE NOT YET AVAILABLE. THE UTILITY REPORTED THAT THE SYSTEM HAS NOT YET PASSED AN ACCEPTANCE TEST.

THE FOLLOWING CUMULATIVE FGD SYSTEM UTILIZATION FIGURES FOR THE PERIOD SEPTEMBER 15 THROUGH DECEMBER 29, 1978 WERE CALCULATED BASED UPON UTILITY REPORTED FGD SYSTEM HOURS FOR THE SAME PERIOD.

A MODULE 22.1% B MODULE 21.7% C MODULE 34.6% D MODULE 34.1% SYSTEM 28.1%

REPORTED FGD SYSTEM HOURS FOR THIS PERIOD WERE 562, 551, 880 AND 868 FOR MODULES A, B, C AND D RESPECTIVELY.

1/79 SYSTEM 744

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

302 FART CHOOKS CHOCKS HOLDER

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS SHUTDOWN ON JANUARY 1, 1979 AS A RESULT OF SEVERE

WINTER WEATHER CONDITIONS.

2/79 SYSTEM 672

3/79 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS DOWN FROM JANUARY 1 TO MARCH 15 DUE TO SEVERE WINTER

WEATHER.

4/79 SYSTEM 722

** PROBLEMS/SOLUTIONS/COMMENTS

DUE TO THE FORMER STACK LINING PEELING AWAY, THE STEEL SHELL WAS SAND BLASTED AND RIGIFLAKE 4850 APPLIED BY TROWEL.

ALL MIST ELIMINATORS WERE CLEANED DUE TO SEVERE SCALING PROBLEMS.

EXTENSIVE REPAIRS WERE MADE TO THE INLET DAMPERS, THE OUTLET DUCTS WERE LINED WITH RESISTIFLAKE 1150, AND MAJOR REPAIRS WERE MADE TO BONNETS BECAUSE OF ACID CORROSION.

THE SYSTEM HAS BEEN DOWN SINCE MID-MARCH FOR INSPECTION AND MAINTENANCE.

5/79 SYSTEM 744

6/79 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE SYSTEM RAN ABOUT THREE DAYS TOTAL DURING THIS THIS PERIOD.

PROCESS CONTROL HAS BEEN A MAJOR PROBLEM AREA SINCE THE SYSTEM BEGAN INITIAL OPERATIONS.

MIST ELIMINATOR PLUGGING CONTRIBUTED TO THE OUTAGE TIME ACCUMULATED DURING THIS PERIOD.

7/79 SYSTEM 744

8/79 SYSTEM 744

9/79 SYSTEM .0 720 0 0 .0

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS SHUTDOWN FOR A SCHEDULED BOILER AND SCRUBBER OVERHAUL IN

SEPTEMBER.

10/79 SYSTEM .0 744 0 0 .0

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS DOWN FOR A SCHEDULED BOILER/TUPBINE/FGD SYSTEM OUTAGE FOR FOUR WEEKS. THE UNIT STARTED UP AGAIN AFTER THE OUTAGE BUT HAD TO SHUTDOWN AFTER ONLY A FEW DAYS BECAUSE OF BOILER PROBLEMS.

INDIANAPOLIS POWER & LIGHT: PETERSBURG 3 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

INSTRUMENTATION IS A CONTINUING PROBLEM. THE MODULE PRESSURE MONITORS.

TO KEEP THE FGD SYSTEM ON LINE FOR MORE THAN 10 DAYS WITHOUT HAVING AT LEAST ONE MODULE FORCED OUT OF SERVICE.

11/79 SYSTEM 720 360

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT CAME BACK ON LINE AGAIN IN MID-NOVEMBER AFTER RESOLUTION OF BOILER PROBLEMS.

AND SOZ AND PH MONITORS ARE ALL INOPERATIVE. THE UTILITY HAS BEEN UNABLE

12/79 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE FOURTH QUARTER THE UTILITY REPORTED THAT THERE WERE NO NEW MAJOR PROBLEMS.

1/80 SYSTEM 744 2/80 SYSTEM 696 3/80 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE FIRST QUARTER OF 1980, THE ENTIRE SCRUBBER PACKING BED WAS LOST DUE TO EXCESSIVE WEAR OF THE NEOPRENE FOAM PACKING BALLS. THE UNIT WILL BE TAKEN OFF LINE IN APRIL TO ACCOMODATE NECESSARY REPAIRS AND REPLACEMENT OF THE BALLS.

BYPASS DAMPER FAILURES ALSO OCCURRED AND ARE REPORTED TO BE A CONTINUAL PROBLEM. MODIFICATIONS WERE MADE TO THE GULLOTINE TYPE DAMPERS DURING THE PERIOD.

 4/80
 SYSTEM
 720

 5/80
 SYSTEM
 744

 6/80
 SYSTEM
 720

** PROBLEMS/SOLUTIONS/COMMENTS

NO INFORMATION WAS AVAILABLE FOR THE PERIOD APRIL 1980 THROUGH JUNE 1980.

7/80 SYSTEM 744 8/80 SYSTEM 744 9/80 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE OPERATIONAL DATA FOR THE THIRD QUARTER 1980 WERE NOT AVAILABLE FOR PUBLICATION.

 10/80
 SYSTEM

 11/80
 SYSTEM

 12/80
 SYSTEM

 720

 744

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT OPERATIONAL DATA FOR FGD OPERATIONS AT PETERS-BURG 3 ARE STILL UNAVAILABLE FOR RELEASE.

1/81 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

DURING JANUARY, ALL OF THE PACKING SPHERES WERE REMOVED FROM THE FOUR ABSORBER MODULES. THE SUPPORTING GRIDS WERE LEFT INTACT AND THE MODULES ARE BEING UTILIZED AS GRID TOWERS.

ALSO DURING JANUARY, REPAIRS TO FREEZE DAMAGED PIPING WERE COMPLETED. THE FRP RECLAIM WATER PIPING WAS RESET IN PLACES WHERE IT HAD PULLED APART AND THE WASTE SLURRY AND SLUDGE TREATMENT WATER LINES WERE THAWED. SOME PIPING GASKETS AND HEAT TRACING CIRCUITS WERE REPAIRED AND UPGRADED. IN ADDITION, SOME DRAIN VALVES WERE ADDED TO IMPROVE THE CAPABILITY TO DRAIN PIPING AND AVOID FUTURE FREEZE DAMAGE.

2/81 SYSTEM 672 3/81 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE FIRST QUARTER, PUMP REPAIRS INCLUDED REBUILDING THE CASING OF A MIST ELIMINATOR WASH PUMP, OVERHAULING A RECYCLE PUMP, AND REPAIRING ONE RECLAIM WATER PUMP AND MOTOR.

 4/81
 SYSTEM
 720

 5/81
 SYSTEM
 744

 6/81
 SYSTEM
 720

** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE SECOND QUARTER, REMAINING PORTIONS OF THE FRP RECLAIM WATER PIPING WERE RESET AND ALIGNED.

SCALE FORMATION WAS REMOVED FROM ALL MIST ELIMINATOR ASSEMBLIES DURING THE SECOND QUARTER.

THE GUNNITE LINING IN THE PRESATURATOR DUCT SECTIONS OF THE FOUR ABSORBER MODULES WERE REPLACED DURING THE THREE MONTH PERIOD.

7/81	SYSTEM	744
8/81	SYSTEM	744
9/81	SYSTEM	720
10/81	SYSTEM	744
11/81	SYSTEM	720
12/81	SYSTEM	744
1/82	SYSTEM	744
2/82	SYSTEM	672
3/82	SYSTEM	744

PERIOD	MODULE AVAILABILI	TY OPERABILITY	PERFORMAN	CE DATA UTILIZATIO	ON % RE	MOVAL	PER	BOILER	FGD	CAP.
9-00-0 0-0					502	PART.	HOURS	HOURS	HOURS	FACTOR
4/82	SYSTEM						720			
5/82	SYSTEM						744			
6/82	SYSTEM						720			
7/82	SYSTEM						744			
8/82	SYSTEM						744			
9/82	SYSTEM						720			
10/82	SYSTEM						744			
11/82	SYSTEM						720			
12/82	SYSTEM						744			
1/83	SYSTEM						744			
2/83	SYSTEM						672			
3/83	SYSTEM						744			
	** PROBLEMS/SOLUT	TIONS/COMMENTS								
		INFORMATION W	AS UNAVAILAB	LE FOR THE	PERIOD	OF JUL	Y 1981	THROUG	H MARCI	H 1983.
4/83	SYSTEM						720			
5/83	SYSTEM						744			
6/83	SYSTEM						720			
	** PROBLEMS/SOLUT	TIONS/COMMENTS								
		INFORMATION W	AS UNAVAILAB	LE FOR THE	PERIOD	OF JUL	Y 1981	THROUG	H JUNE	1983.
7/83	SYSTEM						744			
8/83	SYSTEM						744			
9/83	SYSTEM						720			
	** PROBLEMS/SOLUT									
		INFORMATION W	AS UNAVAILAB	LE FOR THE	THIRD (RUARTER				
	SYSTEM						744			
	SYSTEM						720			
12/03	SYSTEM						744	•		
	** PROBLEMS/SOLUT		14C IBIASIATI 45	LE EOD 7710	FOI MT	011457	n or 3	007		
3 /0/-	SYSTEM	INFORMATION N	BAJIAVANU CA	LC FUR THE	FOURTH	QUARTE				
							744			
	SYSTEM						696			
3/84	SYSTEM						744	•		

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS NOT AVAILABLE FOR THE PERIOD OF JANUARY THROUGH SEPTEMBER OF 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

______ KANSAS CITY POWER & LIGHT COMPANY NAME LA CYGNE PLANT NAME UNIT NUMBER LA CYGNE CITY KANSAS STATE E REGULATORY CLASSIFICATION 55. 1290. **** (.128 LB/MMBTU) (3.000 LB/MMBTU) (****** LB/MMBTU) PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW 1450 GROSS UNIT GENERATING CAPACITY - MW 874 820 GROSS UNIT GENERATING CAPACITY - INNET UNIT GENERATING CAPACITY W/FGD - MW
NET UNIT GENERATING CAPACITY W/FGD - MW 848 EQUIVALENT SCRUBBED CAPACITY - MW 874 ** UNIT DATA - BOILER AND STACK BABCOCK & WILCOX BOILER SUPPLIER CYCLONE BOILER TYPE BOILER SERVICE LOAD BASE DESIGN BOILER FLUE GAS FLOW - CU.M/S
BOILER FLUE GAS TEMPERATURE - C
STACK HEIGHT M 1302.44 (2760000 ACFM) 140.6 (285 F) 213. (700 FT) CONCRETE STACK HEIGHT M STACK SHELL 7.0 (23.0 FT) STACK TOP DIAMETER - M ** FUEL DATA FUEL TYPE COAL FUEL GRADE SUBBITUMINOUS AVERAGE HEAT CONTENT - J/G 21864. (9400 BTU/LB) RANGE HEAT CONTENT - BTU/LB 9000-9700 25.00 AVERAGE ASH CONTENT - % 25.0-35.0 RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - % 8.60 RANGE MOISTURE CONTENT - %
AVERAGE SULFUR CONTENT - % 9.0-10.0 5.39 5.0-6.0 .03 0.02-0.03 RANGE SULFUR CONTENT - %

AVERAGE CHLORIDE CONTENT - %

AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - % *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER Λ TYPE NONE ** ESP NUMBER Ω TYPE NONE ** PARTICLE SCRUEBER NUMBER 8 NUMBER OF SPARES INITIAL START-UP DATE 2/73 GENERIC TYPE VENTURI TOWER SPECIFIC TYPE VARIABLE-THROAT/SIDE-MOVABLE BLOCKS TRADE NAME/COMMON NAME SUPPLIER BABCOCK & WILCOX DIMENSIONS - FT 18.0 X 22.0 SHELL GENERIC MATERIAL STAINLESS STEEL SHELL SPECIFIC MATERIAL AUSTENITIC LINER GENERIC MATERIAL INORGANIC
HYDRAULICALLY-BONDED MORTAR LINER SPECIFIC MATERIAL GAS CONTACTING DEVICE TYPE HOHE 1 315.0 (5000 GPM) 1.9 (14.5 GAL/10 NUMBER OF CONTACTING ZONES LIQUID RECIRCULATION RATE - LITER/S L/G RATIO - LITER/CU.M (14.5 GAL/1000ACF) PH CONTROL ADDITIVE LIMESTONE

2.5 (10.0 IN-H20) 48.8 (160.0 FT/S)

PRESSURE DROP - KPA

SUPERFICIAL GAS VELOCITY M/S

KANSAS CITY POWER & LIGHT: LA CYGNE 1 (CONT.) 162.8 (345000 ACFM) 140.6 (285 F) INLET GAS FLOW RATE - CU.M/S INLET GAS TEMPERATURE - C 22.0 SO2 REMOVAL EFFICENCY - % PARTICLE REMOVAL EFFICIENCY - % 95.0 *** FGD SYSTEM ** GENERAL DATA THROWAWAY PRODUCT SALEABLE PRODUCT/THROWAWAY PRODUCT SO2 REMOVAL MODE WET SCRUBBING LIMESTONE PROCESS TYPE PROCESS ADDITIVES NONE BABCOCK & WILCOX SYSTEM SUPPLIER BLACK & VEATCH A-E FIRM DEVELOPMENT LEVEL FULL SCALE NEW NEW/PETROFIT UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.00 UNIT DESIGN SO2 REMOVAL EFFICIENCY - % EMERGY CONSUMPTION - % CURRENT STATUS 1 6/73 COMMERCIAL START-UP INITIAL START-UP 12/72 CONTRACT AWARDED 3/71 ** DESIGN AND OPERATING PARAMETERS SPACE REQUIREMENTS - SQ M 18765.8 (202000 SQ FT) OPER. & MAINT. REQUIREMENT - MANHR/DAY 300.0 ** QUENCHER/PRESATURATOR MUMBER 0 ** ABSORBER NUMBER 8 NUMBER OF SPARES 0 GENERIC TYPE TRAY TOWER SIEVE TRAY SPECIFIC TYPE TRADE NAME/COMMON TYPE N/A BAECOCK & WILCOX SUPPLIER DIMENSIONS - FT 32.0 X 16.0 X 65.0 SHELL GENERIC MATERIAL STAINLESS STEEL AUSTENITIC SHELL SPECIFIC MATERIAL SHELL MATERIAL TRADE NAME/COMMON TYPE TYPE 316L LINER GENERIC MATERIAL NONE LIMER SPECIFIC MATERIAL N/A LINER MATERIAL TRADE NAME/COMMON TYPE N/A GAS CONTACTING DEVICE TYPE PERFORATED TRAYS NUMBER OF CONTACTING ZONES 2 (48.0IN) (10000 GFH) (41.9 GAL/1000 ACF) DISTANCE BETHEEN GAS CONTACTING ZONES - CM 121.9 LIQUID RECIRCULATION RATE - LITER/S 630. L/G RATIO - L/CU.M 5.6 .7 (3.0 IN-H20) GAS-SIDE PRESSURE DROP - KPA 2.6 SUPERFICAL GAS VELOCITY - M/SEC (8.5 FT/S) (238500 ACFM) (122 F) 112.55 INLET GAS FLOH - CU. M/S INLET GAS TEMPERATURE - C 50.0 502 REMOVAL EFFICIENCY - % 80.0 PARTICLE REMOVAL EFFICENCY - % 95.0 ** HIST ELIMINATOR PRE-MIST ELIMINATOR/MIST ELIMINATOR PRECOLLECTOR MUMBER PER SYSTEM 8 NUMBER OF SPARES PER SYSTEM 0 NUMBER FER MODULE GENERIC TYPE BULK SEPARATION PERFORATED TRAYS SPECIFIC TYPE TRADE NAME/COMMON TYPE SIEVE TRAY BAECOCK & WILCOX MANUFACTURER

HCRIZCHTAL

2.6

1.68 (5.5 FT)

(8.5 FT/S)

1

CONFIGURATION

NUMBER OF STAGES

NUMBER OF PASSES PER STAGE

FPEEBOARD DISTANCE - M SUPERFICAL GAS VELOCITY - M/S

```
CONSTRUCTION MATERIAL GENERIC TYPE
                                               STAINLESS STEEL
                                               AUSTENITIC
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               NONE
   WASH WATER SOURCE
                                               N/A
   WASH FREQUENCY
** REHEATER
                                                8
   NIMBER
                                                n
   NUMBER OF SPARES
                                                1
   NUMBER PER MODULE
                                               IN-LINE
   GENERIC TYPE
   SPECIFIC TYPE
                                               STEAM
                                               BARE TUBE
   TRADE NAME/COMMON TYPE
                                               TOP OF ABSORBER VESSEL
   LOCATION
                                                   .0
   PERCENT GAS BYPASSED - AVG
   TEMPERATURE INCREASE - C
                                                  16.7
                                                               ( 30 F)
    INLET FLUE GAS FLOW RATE - CU. M/S
                                                              ( 238500 ACFM)
                                                 112.55
                                                              ( 122 F)
( 152 F)
    INLET FLUE GAS TEMPERATURE - C
                                                  50.0
    OUTLET FLUE GAS TEMPERATURE - C
                                                  66.7
    NUMBER OF HEAT EXCHANGER BANKS
                                                  4
   NUMBER OF BUNDLES PER BANK
                                                  4
    NUMBER OF TUBES PER BUNDLE
                                                 32
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               STAINLESS STEEL
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               AUSTENITIC
** FANS
   NUMBER
                                                6
    NUMBER OF SPARES
                                                0
    DESIGN
                                               CENTRIFUGAL
    SUPPLIER
                                               WESTINGHOUSE
    FUNCTION
                                               UNIT
                                               INDUCED DRAFT
    APPLICATION
    SERVICE
                                               DRY
    FLUE GAS FLOW RATE - CU.M/S
                                                 207.64
                                                               ( 440000 ACFM)
    FLUE GAS TEMPERATURE - C
                                                 .66.7
                                                              ( 152 F)
    PRESSURE DROP - KPA
                                                   7.0
                                                               (23.0 IN-H20)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL
** FANS
    NUMBER
                                                3
    NUMBER OF SPARES
                                                0
    DESIGN
                                               CENTRIFUGAL
    SUPPLIER
                                               WESTINGHOUSE
    FUNCTION
                                               UNIT
    APPLICATION
                                               FORCED DRAFT
    SERVICE
                                               DRY
    PRESSURE DROP - KPA
                                                               (20.0 IN-H20)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL
** DAMPERS
    NUMBER
                                                B
    FUNCTION
                                               CONTROL
    GENERIC TYPE
                                                LOUVER
    SPECIFIC TYPE
                                               PARALLEL BLADE MULTILOUVER
    MANUFACTURER
    MODULATION
                                               OPEN/CLOSED
    SEAL AIR FLOW - CU. M/S
                                                    .00
                                                               (
                                                                      0 ACFM)
    SERVICE CONDITIONS
                                               285
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               AISI 1110
    LINER GENERIC MATERIAL TYPE
                                               NONE
    LINER SPECIFIC MATERIAL TYPE
                                               N/A
** DAMPERS
   NUMBER
                                                8
    FUNCTION
                                               CONTROL
    GENERIC TYPE
                                                LOUVER
    SPECIFIC TYPE
                                               PARALLEL BLADE MULTILOUVER
   MANUFACTURER
                                               AIR CLEAN
    MODULATION
                                               NR
    SEAL AIR FLOW - CU. M/S
                                                     .00
                                                             (
                                                                      0 ACFM)
    SERVICE CONDITIONS
                                               122
```

0 ACFM)

KANSAS CITY POWER & LIGHT: LA CYGNE 1 (CONT.)

CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE

** DAMPERS

NUMBER
FUNCTION
GENERIC TYPE
SPECIFIC TYPE
MANUFACTURER
MODULATION
MODULATION

SEAL AIR FLOW - CU. M/S SERVICE CONDITIONS CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE

LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE

** DAMPERS

NUMBER
FUNCTION
GENERIC TYPE
SPECIFIC TYPE
MANUFACTURER
MODULATION
SEAL AIR FLOW - CU. M/S
SERVICE CONDITIONS
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
LINER GENERIC MATERIAL TYPE

LINER SPECIFIC MATERIAL TYPE

** DAMPERS

NUMBER
FUNCTION
GENERIC TYPE
SPECIFIC TYPE
MANUFACTURER
MODULATION
SEAL AIR FLOW - CU. M/S
SERVICE CONDITIONS
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

** DUCTWORK

LOCATION

CONFIGURATION
DIMENSIONS
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

** DUCTWORK

LOCATION

CONFIGURATION
DIMENSIONS
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

** DUCTWORK

LOCATION
CONFIGURATION
DIMENSIONS
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE

STAINLESS STEEL AUSTENITIC NONE N/A

8 SHUT-OFF BUTTERFLY N/A NR

OPEN/CLOSED

NR CARBON STEEL AISI 1110 NONE N/A

6 SHUT-OFF LOUVER

PARALLEL BLADE MULTILOUVER

OPEN/CLOSED

.00 (0 ACFM)

175 STAINLESS STEEL AUSTENITIC

NONE N/A

6 SHUT-OFF LOUVER PARALLEL BLADE MUL

PARALLEL BLADE MULTILOUVER

NK.

OPEN/CLOSED

.00 (0 ACFM)

NR
CARBON STEEL
AISI 1110
NONE
N/A

INLET
CIRCULAR, RECTANGULAR
20 FT DIA, 10.5 FT X 10.5 FT
CARBON STEEL
AISI 1110
NONE
N/A

BREECHING TO STACK
CIRCULAR
20 FT DIA
CARBON STEEL
AISI 1110
ORGANIC
INERT FLAKE-FILLED VINYL ESTER

OUTLET
CIRCULAR, RECTANGULAR
12 FT DIA, 13 FT X 13 FT
CARBON STEEL

AISI 1110

```
OPGANTO
     LINER GENERIC MATERIAL TYPE
                                               INERT FLAKE-FILLED VINYL ESTER
     LINER SPECIFIC MATERIAL TYPE
** REAGENT PREPARATION EQUIPMENT
                                               WET BALL MILL
    FUNCTION
                                               COMPARTMENTED
    DEVICE
                                               NO
    DEVICE TYPE
                                               KOPPERS HARDINGE
    MANUFACTURER
                                                2
    NUMBER
    NUMBER OF SPARES
                                                1
    FULL LOAD DRY FEED CAPACITY - M.TONS/HR
                                                  99.9
                                                             ( 110 TPH)
    PRODUCT QUALITY - % SOLIDS
                                                  20.0
** TANKS
                                               NIMBER
    SERVICE
                                                  2
    REAGENT PREP PRODUCT 1
    ABSORBER RECYCLE
                                                  8
    REAGENT PREP PRODUCT 2
                                                  2
    SLURRY BOOSTER HOLD
** PUMPS
                                               NUMBER
    SERVICE
                                                  2
    POND RETURN
    SLURRY FEED
    ABSORBER RECIRCULATION
                                                  A
    SCRUBBER RECIRCULATION
                                                  8
    CLASSIFIER FEED
                                                  4
    SPENT SLURRY BOOSTER
    RECIRCULATION TANK DRAIN
** SOLIDS CONCENTRATING/DEWATERING
    DEVICE
                                               NONE
*** SLUDGE
    MOISTURE CONTENT - % TOTAL FREE WATER
                                                76.0
** TREATMENT
    METHOD
                                               BLEED
    DEVICE
                                               N/A
    PROPRIETARY PROCESS
                                               N/A
 ** DISPOSAL
    NATURE
                                               FINAL
    TYPE
                                                POND
     LOCATION
                                               ON-SITE
    SITE TRANSPORTATION METHOD
                                                PIPELINE
    SITE TREATMENT
                                               NONE
    SITE DIMENSIONS
                                               160 ACRES X 11 FT DEEP
    SITE CAPACITY - CU.M
                                                  2152480 ( 1760.0 ACRE-FT)
 ** DISPOSAL
    NATURE
                                               FINAL
    TYPE
                                                POND
    LOCATION
                                               ON-SITE
    SITE TRANSPORTATION METHOD
                                               PIPELINE
    SITE TREATMENT
                                               NONE
    SITE DIMENSIONS
                                               500 ACRES X 11 FT DEEP
    SITE CAPACITY - CU.M
                                                  6726500 ( 5500.0 ACRE-FT)
    SITE SERVICE LIFE - YRS
                                                10
 ** PROCESS CONTROL AND INSTRUMENTATION
    PROCESS STREAM
                                               VENTURI
    CHEMICAL PARAMETERS
                                               PH
    CONTROL LEVELS
                                               PH 5.6-5.8
    MONITOR TYPE
                                               UNILOC
    MCHITCR LOCATION
                                               VENTURI INLET
    PROCESS CONTROL MANNER
                                               AUTOMATIC
```

KANSAS CITY POWER & LIGHT: LA CYGNE 1 (CONT.)

----- CUENTOTRY NOS-

PROCESS CHEMISTRY MODE	FEEDBACK
** WATER BALANCE WATER LOOP TYPE MAKEUP WATER ADDITION - LITERS/S	OPEN 72.3 (1148 GPM)
	(22.0 0)
** CHEMICALS AND CONSUMPTION FUNCTION NAME PRINCIPAL CONSTITUENT SOURCE/SUPPLIER CONSUMPTION POINT OF ADDITION	ABSORBENT LIMESTONE 91% CACO3, 1% MGCO3 BATES COUNTY ROCK (SUPPLIER) 81 TPH MAX., 70 TPH TYPICAL BALL MILL
** FGD SPARE CAPACITY INDICES SCRUBBER - % ABSORBER - % MIST ELIMINATOR - % REHEATER - % FAN - % BALL MILL - % EFFLUENT HOLD TANK - % RECIRCULATION PUMP - %	.0 .0 .0 .0 17.0 100.0
** FGD SPARE COMPONENT INDICES SCRUBBER ABSORBER MIST ELIMINATOR REHEATER FAN BALL MILL EFFLUENT HOLD TANK RECIRCULATION PUMP	.0 .0 .0 .0 1.0 1.0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

12/72 SYSTEM

THE FIRST TRIAL OPERATION BEGAN ON DECEMBER 26, 1972 AND WAS PLAGUED WITH NUMEROUS PROBLEMS. SOME OF THESE PROBLEMS, SUCH AS VIBRATIONS OF THE INOUCED-DRAFT FANS AND THEIR SENSITIVITY TO IMBALANCE, OCCURRED EVEN BEFORE THE BOILER WAS FIRED. AS THESE FABRICATION PROBLEMS WERE CORRECTED AND THE FGD SYSTEM WENT INTO OPERATION TWO OTHER TYPES OF PROBLEMS APPEARED. THE FIRST TYPE ASSOCIATED WITH THE WET LIMESTONE PROCESS, INCLUDED PLUGGING OF THE MIST ELIMINATORS AND STRAINERS. THE CORROSION ASSOCIATED WITH CONDENSATION OF ACID VAPORS FROM THE GAS ON THE REHEATER TUBE BUNDLES WAS CONTROLLED BY INJECTION OF SLIP STREAMS OF HOT AIR FROM THE BOILER COMBUSTION AIR HEATER INTO THE SCRUBBED FLUE GASES AT THE INLET TO THE REHEATER UNITS. THIS PRACTICE WHICH REDUCED THE MAXIMUM GENERATING CAPACITY OF THE BOILER BY LIMITING THE AIR AVAILABLE FOR COAL COMBUSTION, IS NO LONGER NECESSARY BECAUSE OF SYSTEM DESIGN MODIFICATIONS.

744

6/73	A		20.0				
	В		21.0				
	С		40.0				
	D		21.0				
	E		27.0				
	F		30.0				
	G		23.0				
	SYSTEM	64.0	26.0	720	294	187	15.2
7/73	A		7.0				
	В		24.0				

PERIOD	MODULE	AVAILABILITY	OPERABILITY	PERFORMANCE DATA RELIABILITY UTILIZATION	% REN	IOVAL	PER	BOILER	FGD	CAP.
	C		999000000000	25.0		204.2				
	D			41.0						
	E			27.0						
	F			25.0						
	G			31.0						
	SYSTEM		64.0	26.0			744	303	195	15.2
8/73	A			79.0						
	В			64.0						
	С			65.0						
	D			74.0						
	Ε			47.0						
	F			48.0						
	G			70.0						
	SYSTEM		68.0	64.0			744	699	476	42.1
9/73				13.0						
	В			.0						
	С			13.0						
	D			13.0						
	E			13.0						
	F			.0						
	G			0						
	SYSTEM		53.0	7.0			720	95	50	3.5
10/73				28.0						
	В			41.0						
	С			34.0						
	D			54.0						
	E			33.0						
	F			3.0						
	G			46.0						
	SYSTEM		56.0	34.0			744	452	253	19.7
11/73				48.0						
	В			1.0						
	С			38.0						
	D			4.0						
	E			63.0						
	F			59.0						
	G		F7 A	49.0						
	SYSTEM		57.0	37.0			720	463	266	18.1
12/73				42.0						
	В			20.0						
	C			5.0						
	E			26.0						
	D			31.0						
	F			11.0						
	G		F7 A	32.0						
	SYSTEM		53.0	24.0			744	339	179	10.3
0/74	SYSTEM									
	** PROS	BLEMS/SOLUTION	NS/COMMENTS							

THE 1974 FIGURES ARE BASED UPON ACTUAL SYSTEM OPERATION HOURS AS A FUNCTION OF ACTUAL BOILER HOURS

1/74	A	49.0
	В	32.0
	С	44.0
	D	87.0

ERIOD		BILITY OPERABILITY RELIAS		SO2 PA	RT. HOURS	HOURS	HOURS	FACTOR
	E	23.0	*******			~~~~		
	F	37.0						
	G	81.0						
	SYSTEM	50.0	24.0		744	364	182	6.0
2/74	A	66.0						
C/ 14	B	68.0						
	Ċ	59.0						
	D	76.0						
	E	52.0						
	F	100.0						
	G	65.0						
	SYSTEM	69.0	37.0		672	364	251	16.0
3/74	SYSTEM		.0		744	0	0	.0
	** PROBLEMS/S	OLUTIONS/COMMENTS						
		THE BOILER WAS SHUT	DOWN FOR THE ENTIRE	монтн о	F MARCH.			
4/74		67.0						
	В	70.0						
	С	75.0						
	D	0.88						
	E	74.0						
	F	100.0						
	G	88.0	4				• • •	
	SYSTEM	80.0	37.0		720	332	266	15.0
5/74		69.0						
	В	83.0						
	C D	78.0 85.0						
	E	78. 0						
	F'	84.0						
	G	80.0						
	SYSTEM	80.0	54.0		744	500	400	27.0
6/74	٨	92.0						
0, 14	B	84.0						
	Č	83.0						
	D	90.0						
	E	82.0						
	F	83.0						
	G	87.0						
	SYSTEM	86.0	57.0		720	480	413	32.0
7/74	A	75.0						
	В	80.0						
	C	80.0						
	D	81.0						
	E	85.0						
	F	79.0						
	G	77.0						
	SYSTEM	80.0	34.0		744	313	250	19.0
8/74	A	90.0						
	В	90.0						
	С	73.0						
	D	81.0						
	E	81.0						
	D E F	78.0						
	F G SYSTEM	78.0 99.0	6 5.0		744	571		39.0

PERIOD	MODULE	AVAILABILIT	OPERABILITY	RELIABILITY	UTILIZATION	% RE	MOVAL PART.	PER HOURS	BOILER HOURS		CAP. FACTOR
a /3/											
9/74			69.0								
	8		88.0								
	C		73.0								
	D		76.0								
	E		83.0								
	F		89.0								
	G SYSTEM		86.0 81.0		68.0			720	606	491	36.0
10/74	٨		71.0								
.07 74	B		61.0								
	C		59.0								
	ס										
			81.0								
	E		79.0								
	F		93.0								
	G		89.0								
	SYSTEM		76.0		68.0			744	662	503	39.0
11/74			90.0								
	В		71.0								
	С		60.0								
	D		61.0								
	E		84.0								
	F		85.0								
	G		84.0								
	SYSTEM		76.0		41.0			720	386	293	23.0
2/74	SYSTEM				.0			744	0	0	.0
0./75	SYSTEM								-	·	
0/13	3131611										
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS								
			THE 1975 FIGUT HOURS IN THE H		UPON SYSTEM	I AVAI	LABLE	HOURS /	AS A FU	4CTIOH	OF
1/75	SYSTEM	100.0			.0			744	0	0	.0
	** PROB	BLEMS/SOLUTIO	DNS/COMMENTS								
		•	THE BOILER WAS	S SHUTDOWN DU	JRING JANUARY	AND	FEBRUA	RY FOR	TURBIN	E/GENER	RATOR
			REPAIR.								
2/75	SYSTEM	100.0			.0			672	0	0	.0
3/75		00.0									
3/ /3		82.0									
	В	96.0									
	C	90. 0									
	D	77.0									
	E	93.0									
	F	92.0									
	G	96. 0									
	SYSTEM	89.0						744	694		41.0
	** PROB	BLEMS/SOLUTIO	DNS/COMMENTS								
			DURING REDUCT THEREFORE SHI FOR HIGHER TO	JT DOWN ALTHO	DUGH THEY WER	E AVA	ILABLE	. AVA	E NOT R ILABILI	EQUIRE	D AND THERE-
			. OR HIGHER II	INIT SUITE UP	ine Publeu Fi	LOUKES	THUTC	AIE.			
4/75	SYSTEM	100.0						720			3.4

PERIOD	MODULE	AVAILABILI	TY OPERABILIT	PERFORI Y RELIABILI			1 %	REM	OVAL		BOILER HOURS	FGD HOURS	CAP. FACTOR
	** PROE	BLEMS/SOLUT	IONS/COMMENTS										
			DURING APRIL REPAIRS.	THE BOILER	WAS OFF	LINE	FOR	25	DAYS	DUE TO	NECESS	ARY GEI	NERATOR
5/75	A	95.0											
5/15	B	85.0											
	Ċ	94.0											
	D	90.0											
	E	90.0											
	F	89.0 83.0											
	G System									744	683		56.0
6/75	Δ	88.0											
0, , 5	В	85.0											
	С	84.0											
	ס	85.0											
	Ē	84.0											
	F G	86.0 89.0											
	SYSTEM									720	667		56.0
7./75													
7/75	A B	78.0 90.0											
	C	90.0											
	D	84.0											
	Ε	85.0											
	F	87.0											
	G	85.0								7//	500		E0 0
	SYSTEM	86.0								744	590		50.0
8/75	A	75.0											
	В	88.0											
	C D	87.0											
	E	78. 0 92. 0											
	F	85.0											
	G	83.0											
	SYSTEM	84.0								744	630		50.0
	** PRO	BLEMS/SOLUT	IONS/COMMENTS	;									
			MODULES A A	LD 0 ADE 110	-FD FOR 1					NODI	5 TO 6		r PL 1
			MODULES A A EACH EVENIN	IND D ARE US IG FOR CLEAN		RESEARU	-H II	5515	o. Ur	אב הטטטו	LE 15 5	HOI DO	MN
9/75	A	78.0											
	В	84.0											
	C	84.0											
	D	85.0											
	E F	79.0 78.0											
	Ġ	74.0											
	SYSTEM									720	610		42.0
10/75													
10//5	A B	66.0											
	C	77.0 46. 0											
	Ď	74.0											
	Ε	72.0											
	F	73.0											
	G	65.0								-			17.0
	SYSTEM	68.0								744	231		13.0

		AVAILABILITY				S 02	PART.	HOURS	HOURS	HOURS	FACTOR
						-	646 79				
11/75		93.0									
	В	91.0									
	С	80. 0									
	D.	93.0									
	Ε	96.0									
	F	89.0									
	G	94.0									
		91.0						720	346		29.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
		T!	HE SYSTEM WAS HE GENERATOR	S DOWN OCTOBE AND ID AIR F	R 16 TO NOVE	MBER :	I3 OWIN	NG TO F	ROBLEM	S WITH	
		A T	VAILABILITY F IME FROM OCTO	FIGURES FOR O	OCTOBER AND N	OVEMBI	R DO I	10T INC	LUDE TI	HE OUT	IGE
12/75	Δ	91.0									
14, ,,	B	87.0									
	Č	81.0									
	ם										
	E	85.0									
	_	87.0									
	F	89.0									
	G	84.0									
	SYSTEM	86.0						744	597		47.0
	** PROE	BLEMS/SOLUTION	NS/COMMENTS								
			THREE BOILER	OUTAGES OCCU	RRED DURING	DECEME	BER.				
1/76	A	86.0									
	В	85.0									
	С	91.0									
	D	72.0									
	E	84.0									
	F	82.0									
	G	84.0									
	SYSTEM										
								744	621		51.0
2/76		94.0									
	В	90.0									
	C	86.0									
	Ð	91.0									
	Ε	92.0									
	F	93.0									
	G	95.0									
	SYSTEM	92.0						696	595		55.0
3/76	A	92.0									
	В	90.0									
	c	88.0									
	D	93.0									
	Ē	94.0									
	F	91.0									
	G	91.0									
	SYSTEM	91.0						744	643		57.0
4/76	A	92.0									
	В	91.0									
	C	89.0									
	D	97.0									
	E										
		96.0									

PERIOD	MODULE	AVAILABILIT	Y OPERABILITY RELIABILITY UTILIZATION % REMOVED SOLVED SOL	VAL PER ART. HOURS	BOILER		
	F	98.0					
	G SYSTEM	95.0 94.0		720	143		13.0
	** PROE	BLEMS/SOLUTI	ONS/COMMENTS				
			THE SYSTEM WAS SHUT DOWN ON APRIL 6 FOR A SCHI AND STACK BREECHING OVERHAUL. THE UNIT WAS RE				ATER,
			DURING THE OUTAGE SOME MAINTENANCE WAS PERFORE				TWORK,
			PRIMARILY BECAUSE OF CORROSION PROBLEMS.				
5/76		97.0					
	В	92.0					
	C	94.0					
	D	96.0 89.0					
	E F	9 5.0					
	G	96.0					
	SYSTEM			744	4 436		38.0
	** PRO	BLEMS/SOLUTI	CONS/COMMENTS				
			FROM MAY 10 TO THE END OF THE MONTH FOUR UNI	T OUTAGES	WERE EN	COUNTER	RED.
6/76		93.0					
	₿	94.0					
	C	94.0					
	D	95.0					
	E	92.0					
	F	94.0					
	G SYSTEM	91.0 93. 0		72	0 656		56.0
	** PRO	BLEMS/SOLUT	CONS/COMMENTS				
			FOUR FORCED MINOR SCRUBBER OUTAGES OCCURRED	DURING JU	NE.		
7/76	A	96.0					
	В	95.0					
	С	92.0					
	D	93.0					
	E	93.0					
	F	94.0					
	G SYSTEM	94.0 94.0		74	4 688		60.0
	** PRO	BLEMS/SOLUT	IONS/COMMENTS				
			TWO MINOR SCRUBBER OUTAGES OCCURRED DURING J	ULY.			
			THE UNIT RECORDED ITS LARGEST MW-HOUR MONTH	SINCE INI	HOITAIT	OF COM	MERCIA
			OPERATION (359,028).				
8/76	A	94.0					
8/76	A B	94.0 93.0					
8/76							
8/76	В	93.0					
8/76	B C D E	93.0 92.0					
8/76	B C D E F	93.0 92.0 93.0 92.0 90.0					
8/76	B C D E	93.0 92.0 93.0 92.0		74	4 521		46.0

KANSAS CITY POWER & LIGHT: LA CYGNE 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS TAKEN OUT OF SERVICE AUGUST 24 FOR REPAIR OF A TURBINE BLADE. THE UNIT WAS RETURNED TO SERVICE ON OCTOBER 20. OPERATION WAS INTERMITTENT PENDING TURBINE BLADE REBALANCING AND REESTABLISHMENT OF NORMAL OPERATING CONDITIONS.

DURING THE TURBINE REPAIR PERIOD THE UTILITY COATED THE STACK INNER STRUCTURE WITH PLASTITE 4005.

THE AUGUST AVAILABILITY FIGURES DO NOT INCLUDE THE OUTAGE TIME.

9/76 SYSTEM 100.0 .0 720 0 0 .0

** PROBLEMS/SOLUTIONS/COMMENTS

THE SYSTEM WAS DOWN DUE TO TURBINE REPAIR.

10/76	A	97.0			
	В	97.0			
	С	98.0			
	D	89.0			
	E	96.0			
	F	96.0			
	C D E F G	96.0			
	SYSTEM	96.0		744	254
	3131611	70.0		744	256
11/76	٨	95.0			
11770	A B C D E F	93.0			
	č	94.0			
		95.0			
	ים				
	E -	94.0			
	<u> </u>	91.0			
	G	94.0			
	SYSTEM	94.0		720	627
12/76	A	87.0			
	В	89.0			
	С	81.0			
	D	94.0			
	B C D E F	94.0			
	F	95. 0			
	G	91.0			
	SYSTEM				

** PROBLEMS/SOLUTIONS/COMMENTS

THE A-MODULE VENTURI RECYCLE PUMP EXPERIENCED SOME PROBLEMS AND WAS REPAIRED.

THE C-MODULE REHEAT STEAM TUBE BUNDLES WERE INCREASED IN NUMBER FROM FOUR TO EIGHT.

1/77	A	94.0					
	В	90.0					
	С	95.0					
	D	95.0					
	Ε	95.0					
	F	92.0					
	G	90.0					
	SYSTEM	93.0			744	539	43.0
2/77	A	93.0					

				PERFORMA	NCE DATA						
PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% REI	MOVAL	PER HOURS	BOILER HOURS	FGD HOURS	CAP. FACTOR
	В	93.0									
	С	93.0									
	D	94.0									
	Ε	93.0									
	F	94.0									
	G	88.0									
	SYSTEM	93.0						672	5 9 0		58.0
3/77	A	94.0									
	В	92.0									
	С	86.0									
	ם	94.0									
	Ε	91.0									
	F	94.0									
	G	90. 0									
	SYSTEM	92.0						744	558		50.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE EIGHTH MODULE HAS BEEN INSTALLED.

THE MIST ELIMINATORS IN TWO MODULES HAVE BEEN MODIFIED TO THE POINT WHERE THEY HAVE BEEN OPERATING CONTINUOUSLY CLEAN.

ADDITIONAL BANKS OF STEAM TUBE BUNDLES HAVE BEEN INSTALLED IN SOME MODULES. 50 F OF REHEAT HAS BEEN DETERMINED AS THE NECESSARY TEMPERATURE BOOST AT LA CYGNE TO PRECLUDE STACK PROBLEMS RELATED TO ACID DEW POINT.

THE WATER LOOP IS NOW 95% CLOSED.

A NEW SETTLING POND IS BEING INSTALLED AT THE PLANT.

THE PLANT IS STILL GENERATING 700-720 \mbox{MW} DURING THE DAY AND 500-570 \mbox{MW} AT NIGHT.

4/77	A	96.0					
	В	94.0					
	С	97.0					
	D	94.0					
	Ε	95.0					
	F	96.0					
	G	95.0					
	SYSTEM	95.0			720	384	31.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE EIGHTH MODULE HAS BEEN RUN FOR TWO DAYS.

5/77	SYSTEM	100.0	• 1	0	7-	44 ()	0	.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS SHUT DOWN IN MAY DUE TO TURBINE PROBLEMS. THE UNIT RESTARTED JULY 5, 1977.

THE MIST ELIMATOR WASHING CONFIGURATION IS BEING CHANGED TO WORK COUNTERCURRENT TO THE GAS FLOW.

ADDITIONAL STEAM TUBE BUNDLES ARE BEING ADDED TO INCREASE THE REHEAT AREA.

THE NEW SETTLING POND IS STILL BEING DRAWN UP. EXCAVATION HAS NOT BEGUN.

6/77 SYSTEM 100.0 .0 720 0 0 .0

KANSAS CITY POWER & LIGHT: LA CYGNE 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

MINOR CLEANOUT AND REPAIR WORK WAS DONE ON THE SCRUBBING SYSTEM DURING THE TURBINE OUTAGE.

7/77 A 95.0 93.0 В С 94.0 D 95.0 Ε 95.0 95.0 Ė G 95.0 95.0 н SYSTEM 95.0

744 485 36.0

** PROBLEMS/SOLUTIONS/COMMENTS

RESUMPTION OF OPERATIONS WAS CONDUCTED WITH EIGHT SCRUBBER MODULES IN THE FLUE GAS PATH, ENABLING THE UNIT TO OPERATE AT A MAXIMUM CONTINUOUS LOAD CAPACITY OF 800-820 MW.

89.0 8/77 A В 55.0 С 93.0 D 93.0 Ε 90.0 F 93.0 G 93.0 н 93.0 SYSTEM 87.0

9/77 A

В

С

744 501 43.0

** PROBLEMS/SOLUTIONS/COMMENTS

PARTICLE REMOVAL TESTS WERE CONDUCTED IN LATE AUGUST AND UNIT NO.1 HAS PASSED THE COMPLIANCE REQUIREMENTS (0.13 LB/MM BTU).

MODULE B HAD LOW AVAILABILITY DUE TO THE BURNING OF THE MOTOR ON THE RECIRCULATING PUMP. IT WAS REMOVED FROM SERVICE AND STARTED AGAIN AFTER 12 DAYS.

ם 90.0 Ē 93.0 95.0 F 92.0 н 93.0 SYSTEM 92.0 10/77 Α 91.0 96.0 В С 89.0 94.0 n Ε 93.0 F 94.0 G 89.0 н 93.0 SYSTEM 92.0

93.0

94.0

89.0

720 524 50.0

744 457

3/78 A

В

95.0

95.0

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PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.
                                                    SO2 PART. HOURS HOURS FACTOR
** PROBLEMS/SOLUTIONS/COMMENTS
                     A 12 DAY OUTAGE IN OCTOBER WAS REQUIRED TO DESLAG THE BOILER.
               93.0
11/77
               96.0
     В
               93.0
     С
     D
               94.0
               92.0
     Ε
               93.0
               96.0
     G
     н
               95.0
     SYSTEM
                                                                720
               94.0
                                                                     234
     ** PROBLEMS/SOLUTIONS/COMMENTS
                     THE BOILER WAS SHUT DOWN NOVEMBER 15 BECAUSE OF A NECESSARY TURBINE
                     OVERHAUL. THE BOILER WENT BACK ON LINE DECEMBER 25.
12/77
               98.0
     A
     В
               98.0
     С
               96.0
     ۵
               96.0
     Ε
               96.0
     F
               97.0
     G
               98.0
               99.0
     SYSTEM
               97.0
                                                                     300
                                                                744
     ** PROBLEMS/SOLUTIONS/COMMENTS
                     THERE WERE A FEW SMALL BOILER RELATED OUTAGES IN DECEMBER.
1/78
               90.0
    A
     В
               95.0
     С
               95.0
     D
               95.0
     Ε
               93.0
               94.0
     G
               94.0
     Н
               94.0
     SYSTEM
               94.0
                                                                744
                                                                    597
     ** PROBLEMS/SOLUTIONS/COMMENTS
                     THERE WERE SOME BOILER RELATED OUTAGES IN JANUARY, TOTALING ABOUT 50
                     HOURS.
                     THE FGD SYSTEM CONTINUED TO OPERATE WITHOUT ANY PROBLEMS.
2/78
     A
               92.0
     В
               93.0
     С
               95.0
     D
               94.0
     Ε
               91.0
               97.0
     G
               96.0
               93.0
     SYSTEM
                                                                672 578
                                                                               58.0
               94.0
```

KANSAS CITY POWER & LIGHT: LA CYGNE 1 (CONT.)

- -			 PERFORMA	NCE DATA		 		
PERIOD	MODULE	AVAILABILITY			% RE \$02	PER HOURS		CAP. FACTOR
	c	90.0						
	D	95.0						
	Ε	94.0						
	F	95.0						
	G	89.0						
	H	93.0						
	SYSTEM					744	741	62.0
4/78	A	91.0						
	B	92.0						
	С	93.0						
	D	91.0						
	E	90.0						
	F	92.0						
	G	91.0						
	Н	91.0						
	SYSTEM					720	620	

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER WAS DOWN A TOTAL OF 100 HOURS IN APRIL. THIS TIME INCLUDED THREE OUTAGES DUE TO BOILER LEAKS AND LACK OF LOAD REQUIREMENT.

DURING THE BOILER OUTAGES MODIFICATIONS TO THE FGD SYSTEM INCLUDED CHANGING THE REHEAT TUBE BUNDLES.

5/78	A	89.0
	B	92.0
	С	92.0
	D	93.0
	Ε	92.0
	F	91.0
	G	93.0
	H	86.0
	SYSTEM	91.0

744 593

** PROBLEMS/SOLUTIONS/COMMENTS

IN MAY THE BOILER WAS DOWN TWICE FOR A TOTAL OF 151 HOURS. OUTAGES WERE AGAIN CAUSED BY BOILER LEAKS.

GENERAL MAINTENANCE AND REPAIRS ON THE FGD SYSTEM CONTINUED.

6/78 SYSTEM

720 15

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS UP FOR ONLY 15 HOURS IN JUNE. IN THE FIRST PART OF JUNE THERE WERE BOILER TUBE LEAKS. FROM JUNE 8 TO JUNE 17 A BOILER OUTAGE WAS NECESSARY FOR GENERATOR REPAIR.

7/78	A	88.0		
	В	97.0		
	С	92.0		
	D	94.0		
	Ε	88.0		
	F	93.0		
	G	93.0		
	H	95.0		
	SYSTEM	93.0	744	341
8/78	A	92.0		
	В	93.0		

			 PEDEORMAI	NCE DATA						
PERIOD	HODULE	AVAILABILITY			% REI	MOVAL	PER	BOILER HOURS	FGD	CAP.
	С	95.0								
	D	96.0								
	Ε	93.0								
	F	94.0								
	G	95.0								
	Н	95.0								
	SYSTEM	94.0					744	577		

** PROBLEMS/SOLUTIONS/COMMENTS

THERE WERE TWO BOILER OUTAGES IN AUGUST.

THE UTILITY IS EXPERIMENTING WITH A 3-STAGE MIST ELIMINATOR AND SOME DOUBLE STAGE MIST ELIMINATORS. BETTER MIST ELIMINATION AT THE SCRUBBER EXIT WOULD REDUCE THE FREQUENCY OF REHEATER CLEANING.

9/78	A	96.0		
	В	96.0		
	С	96.0		
	D	96.0		
	Ε	96.0		
	F	96.0		
	G	95.0		
	Н	97.0		
	SYSTEM	96.0	720	720

** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE JULY-SEPTEMBER PERIOD TWO ID FAN ROTERS WERE REPLACED.

```
10/78 A
                  96.0
      В
                  96.0
                  98.0
      С
                  97.0
                  97.0
      Ε
                  98.0
      G
                  97.0
                  96.0
      SYSTEM
                  97.0
                                                                               744 255
```

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO UNUSUAL OPERATING PROBLEMS WERE ENCOUNTERED DURING OCTOBER AND NOVEMBER.

11/78	A	92.0				
	В	95.0				
	С	94.0				
	D	93.0				
	E	94.0				
	F	93.0				
	G	94.0				
	Н	96.0				
	SYSTEM	94.0			720	720

** FROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO UNUSUAL OPERATING PROBLEMS WERE ENCOUNTERED DURING OCTOBER AND NOVEMBER.

12/78	A	93.9
	В	92.9
	С	94.0

KANSAS CITY POWER & LIGHT; LA CYGNE 1 (CONT.)

					UTILIZATION	502	PART.	HOURS	HOURS	HOURS	FACTOR
~=~~~		0E A									
	D E	95.0 94.7									
	F	79.7									
		90.5 94.4									
	G	94.4									
	Н										
	SYSTEM	93.8						744	239		
1/79	A	95.6									
•	В	96.5									
	C	97.2									
	D	96.3									
	E	90.7									
	F	97.2									
	G	97.2									
	H	95.4 95.8						744	205		
								, , ,	243		
	** PROE	BLEMS/SOLUTIO									
			DURING THE DI BOILER OUTAGE		ARY PERIOD TH	E UNI	T EXPE	RIENCE) A MUL	TITUDE	OF
2/79	٨	95.0									
2/17											
	В	94.6									
	C	92.6									
	D	93.5									
	E	95.1									
	F	94.3									
	G	94.1									
	Н	93.8									
	SYSTEM	94.1						672	342		
3/79	A	96.1									
	В	96.0									
	С	93.2									
	D	95.6									
	Ē	96.5									
	F	94.8									
	G	95.7									
	Н										
		93.4 95.2						344	73.6		
	3131211	75.2						/44	314		
	** PROE	BLEMS/SOLUTIO	NS/COMMENTS								
		N F	O MAJOR FGD :	SYSTEM PROBLI	EMS WERE REPO	RTED I	BY THE	OTILI.	TY FOR I	FEBRUA	RY OR
			THE UTILITY H		THAT MANY TUB ER.	E LEA	KS AND	CYCLO	NE LEAK	S WERE	
4/79	A	95.5									
	B	95.7									
	C	94.4									
	D	91.4									
	E	95.5									
	F	96.2									
	G	95.9									
	Н	95.7									
	SYSTEM	95.0						720	638		
E /70		6 . -									
5/79	д	96.5									

ERIOD			Y OPERABILITY			% RE	MOVAL	PER			
	D	95.3									
	E	95.4									
	F	95.7									
	G	96.3 95. 5									
	H SYSTEM							744	476		
	** PROBL	EMS/SOLUT	ONS/COMMENTS								
			THE UTILITY R	EPORTED THAT	NO MAJOR FGD	PROB	LEMS H	AD OCC	JRRED.		
6/79	SYSTEM	100.0			.0			720	0	0	.0
	** PROBL	EMS/SOLUT	ONS/COMMENTS								
			THE UNIT WAS I							CHEDUL	ED
7/79	SYSTEM	100.0			.0			744	0	0	
	** PROBL	EMS/SOLUT	ONS/COMMENTS								
			THE TURBINE WAINTENANCE WA						AGE SOM	E MINO	R
8/79		86.8									
	В	95.9									
	С	96.3						2.			
	D E	96.3 95.9						_			
	F	95.9 96.2									
	G	88.5									
	H	96.9									
	SYSTEM	94.1						744	231		
9/79	A	96.0									
	В	96.1									
	С	95.6									
	ם	94.3									
	E	96.7									
	F	96.1									
	G H	96.0 96.9									
	SYSTEM	96.0						720	618		
	** PROBL	.EMS/SOLUT	ONS/COMMENTS								
			THE FGD UNITS WAS PERFORMED				MS AND	ONLY	REGULAR	MAINT	ENANCE
0/79	A	95.3									
	В	95.8									
	С	94.7									
	ם	92.7									
	E	94.4									
	F	94.9									
	G H	94.7									
	SYSTEM	94.5 94.6						744	436		
L/79	SYSTEM	. 0			.0			720	0	0	.0
2/79	SYSTEM	. 0			.0			744	0	0	.0

KANSAS CITY POWER & LIGHT: LA CYGNE 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER WENT DOWN FOR AN OVERHAUL ON OCTOBER 19 AND WAS OUT OF SERVICE THROUGH DECEMBER.

EXTENSIVE MAINTENANCE WORK BEGAN ON THE FGD SYSTEM LATE IN OCTOBER CAUSING THE SYSTEM TO BE UNAVAILABLE DURING NOVEMBER AND DECEMBER. SOME ITEMS INCLUDED IN THE MAINTENANCE WERE:

THE INSTALLATION OF TWO NEW SPRAY HEADERS IN SIX OF THE MODULES, RE-PLACEMENT OF THE ABSORBER SIDEWALLS, REPLACEMENT OF THE MODULE OUTLET DUCTS AND DAMPERS, AND VARIOUS DUCTWORK PATCHING.

1/80 SYSTEM .0

.0 744 0 0 .0

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER AND FGD SYSTEM REMAINED UNAVAILABLE DURING JANUARY DUE TO THE ON-GOING GENERATOR/TURBINE OVERHAUL AND THE EXTENSIVE FGD SYSTEM MOD-IFICATIONS BEING PERFORMED.

2/80	A	98.2	84.1	95.7	20. 0				
	В	98.2	58.3	92.9	13.2				
	С	97.4	66.2	89.7	14.9				
	D	99.1	45.9	92.3	10.3				
	E	98.2	93.0	97.3	21.0				
	F	99.1	91.7	97.3	20.7				
	G	99.1	91.7	97.3	20.7				
	Н	99.6	92.4	97.3	20.8				
	SYSTEM	98.6	7 7.7	95.3	17.5	696	157	122	10.9

** PROBLEMS/SOLUTIONS/COMMENTS

THE TURBINE/GENERATOR OVERHAUL WAS COMPLETED IN FEBRUARY AND THE BOILER AND FGD SYSTEM RETURNED TO SERVICE ON FEBRUARY 20. THE FGD SYSTEM WAS AVAILABLE FOR OPERATION MOST OF THE MONTH.

3/80	A	94.6	100.0	100.0	4.3
	В	96.2	100.0	100.0	4.3
	С	96.1	100.0	100.0	4.3
	D	96.1	100.0	100.0	4.3
	Ε	95.8	93.8	100.0	4.0
	F	94.7	53.1	100.0	2.3
	G	93.3	31.3	100.0	1.3
	Н	95.7	.0		.0
	SYSTEM	95.3	72.3	100.0	3.1

744 32 23 1.7

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS OPERATED FOR ONLY 23 HOURS IN MARCH AS A RESULT OF GENERATOR/TURBINE PROBLEMS. SOME ROUTINE CLEANING AND INSPECTIONS OF THE FGD SYSTEM WERE PERFORMED DURING THE OUTAGE TIME.

4/80	A	96.3	94. 1	94.5	61.7				
	В	95.1	78.4	91.4	51.4				
	С	95.0	97.5	92.9	63.9				
	D	96.7	93.6	94.8	61.4				
	E	95.3	86. 0	92.3	56.4				
	F	92.5	76. 3	87.2	50. 0				
	G	97.0	68.4	93.9	44.9				
	Н	97.0	62.9	93.4	41.3				
	SYSTEM	95.6	82.2	92.6	53.9	720	472	388	37.6
5/80	A	96.4	89.4	96.0	84.1				

KANSAS CITY POWER & LIGHT: LA CYGNE 1 (CONT.)

				PERFORMAN	ICE DATA						
PERIOD		AVAILABILITY				S02	PART.	HOURS	HOURS	HOURS	FACTOR
	В										
	C	95.7	88.3	93.9 95.2 95.1 95.3	83.1						
	D	95.9	83.9	95 1	78 9						
	E	96.1	84.4	95 3	79.4						
	F	96.5	89.3	94.2	84.0						
		96.1	96.0	96.2 94.0	90.3						
	G H	70.1	70.0	96.2	70.3						
	•••	96.0 96.0			77.4 82.5			744	700	49%	40.0
	3131611							744	700	014	49.9
6/80	A	98.2	89.5	97.2	46.0						
	В	98.1	90.3	96.8	46.4						
	С	97.4	96.8	96.7 98.0	49.7						
	D	98.1	92.5	98.0	47.5						
	E	98.1	87.6 91.1	97.9 98.5	45.0						
	F	98.3	91.1	98.5	46.8						
	G	98.8	88.2	97.3	45.3						
	Н	99.3	87.3	97.3 98.6	44.9						
	SYSTEM	98.3	90.4	98.9	46.4			720	370	334	35.5
	** PRO	BLEMS/SOLUTIO	NS/COMENTS								
		N	O MAJOR FGD I	RELATED PROBL	EMS WERE REF	ORTED	FOR T	HE SEC	AUP GNC	RTER OI	F 1980.
7/80	A	89.7	86.9	87.1	69.9						
	B	97.8	97.6	97.3	78.5						
	Č	97.3	96.9	96.6	77.9						
	D	98.1	98.0	97.7	77.9 78.8						
	E		90.0	97.8	70.0						
		98.2	97.6	97.8	78.4						
	F	98.6	98.6	98.3 97.6	79.3						
	G	98.1	97.9	97.6	78.7						
	Н	97.7	96.9	97.1 96.2	77.9						
	SYSTEM	96.9	96.3	96.2	77.4			744	5 98	576	60.9
	** PRO	BLEMS/SOLUTION	NS/COMMENTS								
		N	O MAJOR FGD-	RELATED PROBL	EMS WERE REP	ORTED	FOR J	ULY.			
8/80	A	94.6	92.7	93.9	66.9						
	В	97.9	97.3	97.2	70.3						
	С	98.1	^- ~	^7 7	70.3						
	D	97.7	96.8	97.3 97.4 96.7	69.9						
	E	97.2	96.2	96.7	69.5						
	F	98.7	97.2	98.1	70.2						
	G	97.6	96.9	96.7	69.9						
	H		96.4								
	SYSTEM	97.4	96.4	96.7	69.6			744	537	518	54.7
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			HE UTILITY RI	EPORTED THAT	NO MAJOR PRO	BLEMS	WERE	ENCOUN	TERED D	URING '	THE
9/80		00.0	00. 4	00 0	F7 0						
<i>,,</i> 90		98.9	90.4	98.0	53.9 54.7						
	В	98.6	91.1	97.5	54.3						
	C	97.8	90.7	96.0	54.0						
	D	94.9	84.8	90.8	50.6						
	E	9 8.6	91.1	97.5	54.3						
	F	99.2	93.0	98.5	55.4						
	G	99.2	93.0	98.5	55.4						
	Н	98. 8	90.2	97.7	53.8						
	SYSTEM	98.2	90.7	97.0	54.0			720	429	389	43.3
				•				•	,		

KANSAS CITY POWER & LIGHT: LA CYGNE 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS TAKEN OFF LINE SEVERAL TIMES FOR A TOTAL OF 118 HOURS BECAUSE OF BOILER TUBE LEAKS.

THE BOILER WENT DOWN ON SEPTEMBER 27, 1980 FOR A SCHEDULED MAINTENANCE OVERHAUL. THE FGD SYSTEM WAS AVAILABLE DURING THIS TIME.

10/80 SYSTEM 100.0

.0 744 0 0 .0

** PROBLEMS/SOLUTIONS/COMMENTS

DURING OCTOBER THE BOILER REMAINED OUT OF SERVICE DUE TO AN ANNUAL TURBINE/BOILER OVERHAUL. THE FGD SYSTEM WAS AVAILABLE DURING THIS TIME.

11/80	A	99.9	92.1	98.3	8.0				
	В	100.0	100.0	100.0	10.0				
	С	100.0	100.0	100.0	10.0				
	D	90.0	.0	.0	. 0				
	E	100.0	100.0	100.0	10.0				
	F	100.0	100.0	100.0	10.0				
	G	99.7	85.7	96.4	7.5				
	н	100.0	59.5	100.0	5.2				
	SYSTEM	87.5	87.3	85.9	7.6	720	63	55	8.7

** PROBLEMS/SQLUTIONS/COMMENTS

DURING NOVEMBER THE BOILER WAS IN SERVICE APPROXIMATELY 63 HOURS DUE TO THE ANNUAL TURBINE/BOILER OVERHAUL. THE FGD SYSTEM WAS AVAILABLE 98.7% DURING THIS TIME.

MODULE D WAS OUT OF SERVICE DUE TO REPAIRS CAUSED BY FIRE DAMAGE RECEIVED ON OCTOBER 13, 1980.

12/80	A	97.8	96.7	96.9	66.7				
	В	98.0	96.3	97.0	66.4				
	С	98.1	97.1	97.3	66.9				
	D	. 0	.0	.0	۰.0				
	Ē	98.5	97.7	97.8	67.3				
	F	98.2	93.8	97.4	64.6				
	G	95.2	90.6	92.8	62.5				
	н	98.9	93.6	98.1	64.5				
	SYSTEM	85.6	93.6	98.1	64.5	720	513	427	45.2

** PROBLEMS/SOLUTIONS/COMMENTS

MODULE D REMAINED OUT OF SERVICE THE ENTIRE MONTH DUE TO THE NECESSARY REPAIRS CAUSED BY FIRE DAMAGE IN OCTOBER.

THE UTILITY REPORTED NO MAJOR FGD-RELATED PROBLEMS OCCURRED DURING THE MONTH OF DECEMBER.

1/81	A	96.9	100.0	96.1	76.5				
	В	94.1	100.0	92.9	76.7				
	С	94.4	100.0	93.2	77.0				
	D	18.3	1.5	1.1	1.0				
	E	95.8	100.0	94.9	76.9				
	F	97.0	100. 0	96.4	78. 6				
	G	96.8	100.0	96.1	79.4				
	Н	97.2	100.0	96. 6	79.8				
	SYSTEM	86.6	100.0	83.3	68.3	744	465	508	62.5
2/81	A	99.6	100.0	99.4	72.0				

744 633 605 68.7

В	99.3	100.0	98.8	68.0					
С	99.4	99.7	99.1	65.2					
D	99.3	100.0	99.0	72.9					
E	99.1	93.1	98.5	60.9					
F	99.1	92.9	98.6	60.7					
G	99.7	95.2	99.4	62.2					
H	99.6	100.0	99.2	66.2					
SYSTEM	99.4	100.0	99.1	66.1		672	439	444	47.3
	LEMS/SOLUTIO	10 /00 /4E ITO							

3/81	A	97.2	100.0	96.9	86.9	
	В	97.7	96.5	97.3	82.1	
	С	95.6	100.0	95.1	85.8	
	D	96.8	96.1	96.2	81.2	
	E	97.2	98.4	96.7	83.7	
	F	97.8	89.8	97.3	76. 5	
	G	97.3	93.3	96.7	79.4	
	H	97.7	87.3	97.0	74.3	
	SYSTEM	97.2	95.5	96.6	81.3	

^{**} PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO OTHER MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE FIRST QUARTER 1981.

4/81	A	97.4	97.3	94.5	45.7				
	В	97.5	98.2	94.9	46.1				
	С	97.1	97.3	94.0	45.7				
	D	97.2	97.6	94.0	45.8				
	Ε	97.4	97.3	94.5	45.7				
	F	97.4	97.6	94.3	45.8				
	G	97.4	97.6	94.6	45.8				
	H	97.1	96.7	94.0	45.4				
	SYSTEM	97.3	97.5	94.4	45.8	720	338	330	36.1
5/81	A	99.7	53.3	94.1	5.4				
	В	99.7	81.3	96.8	8.2				
	С	100.0	84.0	100.0	8.5				
	D	100.0	84.0	100.0	8.5				
	E	100.0	33.3	100.0	3.4				
	F	100.0	.0		.0				
	G	100.0	.0		.0				
	Н	100.0	.0		.0				
	SYSTEM	99.9	42.0	98.2	4.3	744	75	32	12.6
6/81	A	99.7	100.0	98.6	19.6				
	В	99.3	100.0	96.5	19.2				
	С	99.0	100.0	94.3	16.0				
	D	99.2	100.0	95.8	19.0				
	Ε	79.4	20.2	12.9	3.1				
	E F	99.6	100.0	97.9	19.3				
	G	99.9	20.6	95.8	3.2				
	н	100.0	.0		.0				
	SYSTEM	97.0	67.6	84.5	12.4	72	109	89	4.0

^{**} PROBLEMS/SOLUTIONS/COMMENTS

DURING JUNE, MODULE E WAS UNAVAILABLE FOR 572 HOURS AS A RESULT OF PROBLEMS ENCOUNTERED WITH THE VENTURI PUMP MOTOR.

KANSAS CITY POWER & LIGHT: LA CYGNE 1 (CONT.)

				PERFORMAI	NCE DATA						
PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% RE	MOVAL	PER	BOILER	FGD	CAP.
7/81	A	96.9	95.8	95.4	64.2						
,, 01	B	97 2	95.8 93.0	95.7	64.2 62.4						
	C	97.4	73.0	95 1	49.6						
		96.0	80.4	95.1 93.7	59.9						
	Ď	96.1	07.4	93.7	55.1						
	Ē		02.2	93.4 95.8	22.1						
	F	98.0	69.1	95.8	46.4						
	G	97.2	75.8	95.0	50.8						
	H	98.0 97.2 97.8 97.1	60.5	95.0	40.6						
	SYSTEM	97.1	80.0	94.9	53.6			744	499	399	37.0
8/81	A	94.4	100.0	93.3							
	В	95.9	100.0	95.4	86.0						
	С	93.1	100.0	91.3	72.5						
	D	94.9 94.3	100.0	94.0 92. 5	79.9						
	Ε	94.3	97.5	92. 5	70.4						
	F	96.2	100.0 99.4	95.0	73.2						
	G	95.9	99.4	94.7	71.8						
	н	96.4	93.4	94.9							
	SYSTEM	96.4 95.1	100.0	95.1	67.4 74.9			744	537	557	57.7
0.403		74 /									
9/61	A		100.0	91.2	27.9						
	В	29.5	100.0	88.5 94.8	29.5 31.6						
	C	31.6	100.0	94.8							
	D	30.4	100.0 97.8	91.3	30.2 26.9						
	E	32 .3	97.8	96.1	26.9						
	F	32.3	100.0	96.6	30.5						
	G	32.4	95.6	96 . 6	26.3						
	H	32.9	83.7	98.4	23.0						
	SYSTEM	32.3 32.4 32.9 31.5	100.0	93.9	28.4			720	198	203	13.8
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
					NO MAJOR FGO	-RELA	TED PR	DBLEMS	WERE EI	NCOUNTE	ERED
		٥	URING THE MOI	ATHS OF JULY	AND AUGUST.						
			URING SEPTEM VERHAUL.	BER THE FGD :	SYSTEM WAS OF	F-LIN	E 504 I	HOURS	FOR A S	CHEDULI	ED
10/81		50.8	100.0	97 .9	40.3						
	В	48.3	100.0	92.6	41.7						
	С	51.4	100.0 100.0	99.4	40.9						
	D	51.6	100.0	100.0	42.0						
	Ε	48.3	83. 8	98.8	30.0						
	F	47.3	90.0	99.3	32.2						
	G	51.5	74.3	99.8	26.6						
	Н	51.5	72.9	99.7	26.1						
	SYSTEM	50.6	97.9	98.2	35.0			744	266	260	19.3
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
		D	URING OCTOBE	R THE SYSTEM	WAS OFF-LINE	345	HOURS	то сом	PLETE A	SCHED	ULED
		0	VERHAUL.								
11/81	A	97.4	100.0	97.0	85.6						
	В	95.9	100.0	95.1	79.6						
	С	92.3	100.0	90.3	71.8						
	D	92. 9	100.0	91.8	79.8						
	E	96.0	100.0	94.6	69.6						
	F	90.1	97.3	86.4	62.7						
	G	94.1	98.4	91.6	63.4						
	н	91.8									
	SYSTEM	93.8	100.0	89.1	66.9			70.0	,,,		49 1
	J.JILII	73.0	100.0	92.1	72.4			72 0	464	521	41.6

_			OPERABILITY			SO2 PA	RT.	HOURS	HOURS	HOURS	FACTO
	** PRO	SLEMS/SOLUTIO	NS/COMMENTS								
			URING NOVEMBI ERE ENCOUNTER		TY REPORTED T	HAT NO M	AJOR	FGD-R	ELATED	PROBLE	MS
12/81	A	96.4	100.0	95.6	78.7						
	В	93.4	100.0	91.0	66.6						
	Ċ	98.7	100.0	98.0	64.9						
	ם	98.2	100.0	97.2	62.5						
	Ē		100.0	98.6 97.4	51.5						
	F	98.7	94.2	97.4	46.4						
	G	99.1	07.0	^^ ^	41.1						
	H	99.4	73.3	98.4	36.2						
	SYSTEM		93.8	98.0 98.4 96.8	56.0			744	386	417	25.9
				75.0	2010				300	,-,	2217
	** PRUI	BLEMS/SOLUTIO									
			HE UTILITY RI ECEMBER.	EPORTED THAT	NO MAJOR FGD	PROBLEM	S WE	RE ENC	OUNTER	ED DURI	ING
1/82	A	88.0	78.5	81.8	53.9						
	В	93.2	98.7	90.9	67.8						
	С	95.9	100.0	95.2	80.1						
	D	91.5	300 0	89.2	70.3						
	E	92.3	83.1	88.2	57.1						
	F	85.0	94.7	88.2 81.2	65.0						
	G	07.0	75 4	0/ E	F2 0						
	H	97.3	100.0	96.5	73.2						
	SYSTEM	92.5	100.0	89.7	64.9			744	511	483	33.4
2/82		94.7 96.9	100.0 100.0	92.1 95.7	60.9						
	В			95.7	68.1						
	С	96.8	100.0	95.3	64.8						
	D	98.1	100.0	97.0 93.7	64.0						
	E	95.7	100.0	93.7	62.8						
	F	95.5	83.2	90.6	43.1						
	G	96.5	73.8	91.6	38.2						
	н	97.1	67.4	92.2	34.9						
	SYSTEM	96.4	90.6	93 .5	58.3			672	348	367	24.0
3/82	A	97.3	100.0	96.6							
	В	95.1	100.0	93.2	67.7						
	C	96.4	100.0	95.0	69.2						
	D	91.5	100.0	87.8	61.0						
	Ę	95.2	95.8 100.0 59.0	92.1	56. 8						
	F	98.0	100.0	100.0	96.8						
	G	95.4	59.0	88.4	35.0						
	H	97.7	95.3	96.1	56.5						
	CVCTEM	95.8	07.0					744	443	440	33.3

** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE FIRST QUARTER 1982 THE UTILITY REPORTED EXPERIENCING NO MAJOR FGD-RELATED PROBLEMS.

4/82	A	97.7	100.0	94.9	42.4
	В	98.5	100.0	96.4	41.3
	С	99.2	100.0	98.2	42.4
	D	98.9	100.0	97.4	41.2
	Ε	99.0	100.0	97.6	40.3
	F	99.7	96.9	99.2	38.0
	G	99.4	68.1	97.9	26.7

KANSAS CITY POWER & LIGHT: LA CYGNE 1 (CONT.)

ERIOD	MODULE A	VAILABILIT)	Y OPERABILITY			502	PART.	HOURS	HOURS	HOURS	
		98.7									~~~~
	SYSTEM	98.9	92.4 94.7	97.3	38.6			720	282	278	20.5
	** PROBL	EMS/SOLUTIO	ONS/COMMENTS								
		(ON APRIL 16 TI	HRU APRIL 30	THE UNIT WAS	OUT	OF SERV	/ICE FO	OR AN O	VERHAUI	L.
5/82	SYSTEM	100.0			.0			744	0	0	.0
	** PROBL	EMS/SOLUTIO	ONS/COMMENTS								
		τ	DURING MAY THE DURING THIS T HOWEVER, THE	ME GENERAL	MAINTENANCE F	IAS PE	RFORME	וד אס כ	HE FGD		
6/82	A	99.2		97.1	25.8						
	В	98.7	100.0	95.8	30.2						
	Ċ	95.0	98.2	84.3	26.9						
	D	99.5	98.2 100.0	98.7	36.3						
	E F	77.3	70.0	70.1	24.6						
	G	89.9 99.2		97.7	18.8 34.8						
	Н		100.0		31.9						
		97.5	93.9	91.7	28.7			720	197	206	13.0
	** PROBL	EMS/SOLUTIO	DNS/COMMENTS								
			THE UTILITY REDURING JUNE.	EPORTED THAT	NO MAJOR FGD	-RELA	TED PRO	OBLEMS	WERE E	NCOUNTE	ERED
7/82	A	97.5	100.0	97.4	90.9						
	В			94.9							
	С	95.8	100.0 100.0	95.3	85.8 86.3						
	D	97.1	100.0	96.7	85.4 79.4						
	Ε	98.1	98.5	97.7	79.4						
	F	95.1	92.2 97.7	93 A	74.3						
	G	97.3	97.7	96.7	74.3 78.8						
	H	97.3	100.0 100.0	96.9	03.2						
	SYSTEM	96.7	100.0	96.2	83.0			744	600	618	53.8
8/82	A	98.0	100.0	97.6	82.6						
	В	96.9	100.0 100.0	96. 6	86.7						
	С	97.6	100.0	97.4	86.9						
	D	97.3	100.0	96. 9	83.1						
	E	98.7	100.0	98.5	86.3						
	F	98.1	100.0	97.8	85.4						
	G	96.7	100.0	96.2	83.0						
	H SYSTEM	98.5 97.7	99.0 100.0	98.1 97.4	76.4 83.8			744	574	623	46.2
9/82	A	92.1	100.0	90.7	77.2						
	В	97.2	100.0	96.3	72.0						
	С	96.2	100.0	95.3	77.3						
			100.0	89.7	72.5						
	D	71./		- / + ;	,						
	D E	91.7 98.0		97.2	71 n						
		98.0	100.0	97.2 96.1	71. 0 70.1						
	Ε		100.0 100.0	96.1	70.1						
	E F	98.0 97.2	100.0								

KANSAS CITY POWER & LIGHT: LA CYGNE 1 (CONT.)

	MODULE AV	AILABILITY	OPERABILITY R	ELIABILITY	UTILIZATION				BOILER HOURS		CAP.
	** PROBLE	MS/SOLUTIO	NS/COMMENTS								
		т	HE UTILITY REP	OPTED THAT	NO MAIOD FOR	1_DF1 AT	EN DOC	RI FMS	MEDE E	ארטו ואדו	DEN
			URING THE JULY			J-KELA I	בט דאנ	סנבווס	MCKE E	1000111	בתבט
0/82	A	97.0	100.0	96.2	76.0						
	В	96.8	100.0	95.6	70.4						
	С	97.0	100.0	96.1	74.1						
	D	97.8	100.0	97.2	74 3						
	Ε	98.4	100.0	97.6	68.0						
	F	98.5		97.7 96. 9	64.4						
	G	98.1	100.0 100.0	96.9	59.8						
	н			95.7	63.0						
	SYSTEM	97.6	100.0 100.0	96.6	68.8			744	440	512	35.2
	** PROBLE	MS/SOLUTIO	NS/COMMENTS								
		И	O MAJOR FGD-RE	LATED PROBL	EMS WERE REF	PORTED	BY THE	UTIL:	ΙΤΥ		
		D	URING OCTOBER.								
			70.0								
1/82			79.2	99.0							
	В	13.2	79.2	99.5	13.2						
	С			98.5	13.1						
	ם	12.8	76.7	96.5	12.8						
	Ε	12.8	77.1	95.9	12.8						
	F	12.8	77.1	96.7	12.8						
	G	12.8	76.7	95.8	12.8						
	Н	13.3	79.6	99 5	17.7						
	SYSTEM	13.0	78.0	97.7	13.0			720	120	94	11.
	** PROBLE	MS/SOLUTIO	NS/COMMENTS								
		т	HE UTILITY REF	ORTED TURBI	NE GENERATOR	R PROBL	.EMS DI	JRING N	10VEMBE	₹.	
2/82	SYSTEM	.0			. 0			744	0	0	. (
1/83	SYSTEM	.0			.0			744	0	0	. (
2/83	SYSTEM	.0			.0			672	0	0	. (
3/83	SYSTEM	.0			.0			744	0	0	. (
	** PROBLE	MS/SOLUTIO	NS/COMMENTS								
			HE UNIT WAS TA		_				OR AN E	XTENDE)
										_	. (
4/83	SYSTEM	.0			.0			720	0	0	• '
4/83			NS/COMMENTS		.0			720	0	0	• `
4/83		MS/SOLUTIO T I	NS/COMMENTS HE UNIT WAS DO NCLUDED THE RE YCLONES.		APRIL DUE TO			BOILER	REPAIR	S. REI	
		MS/SOLUTIO T I	HE UNIT WAS DO		APRIL DUE TO			BOILER	REPAIR: , AND S	S. REI	PAIRS

KANSAS CITY POHER & LIGHT: LA CYGNE 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE SCHEDULED OUTAGE CONTINUED THROUGH THE SECOND QUARTER OF 1983 WITH TURBINE AND GENERATOR WORK BEING COMPLETED.

7/83	A	60.1	91.1	96.1	45.3		
	В	61.2	88. 6	92.8	44.1		
	С	61.7	95.4	94.5	47.4		
	D	62.9	94.3	96.9	46.9		
	Ε	63.3	93.5	97.7	46.5		
	F	62.8	82.4	96.2	41.0		
	G	63.3	99.2	97.6	49.3		
	н	63.7	92.7	98.4	46.1		
	SYSTEM	62.4	92.2	96.3	45.8	744	370

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY ATTRIBUTED LOW BOILER HOURS DURING JULY TO START-UP TIME AND TESTS REQUIRED FOLLOWING THE EXTENDED OUTAGE.

341

8/83	A	76.1	100.0	98.1	68. 0				
	В	76.2	100.0	98.3	68.1				
	С	75. 7	100.0	97.6	67.6				
	D	75.9	100.0	97.8	65.9				
	E	75.4	98.1	97.0	62. 5				
	F	75.9	94.7	97.6	60.3				
	G	75.4	94.9	96.8	60.5				
	Н	76 . 6	94.5	98.6	60.2				
	SYSTEM	75.9	97.8	97.7	64.1	744	474	477	17.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY ATTRIBUTED LOW FGD SYSTEM AVAILABILITY DURING AUGUST TO CONTINUED TESTING ON THE BOILER AND SCRUBBER.

•	9/83	A	.0			
		В	.0			
		C	.0			
		D	.0			
		E	.0			
		F	.0			
		G	.0			
		Н	.0			
		SYSTEM	.0	720	0	.0

** PROBLEMS/SOLUTIONS/COMMENTS

A FORCED OUTAGE OCCURRED DURING SEPTEMBER DUE TO TURBINE GENERATOR PROBLEMS. THE UTILITY HOPED TO BE BACK IN SERVICE BY NOVEMBER, 1983.

10/83	SYSTEM	744
11/83	SYSTEM	720
12/83	SYSTEM	744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS DOWN THE ENTIRE FOURTH QUARTER OF 1983 DUE TO CONTINUED BOILER AND TURBINE REPAIRS. THE UTILITY HOPES TO BE BACK IN SERVICE BY THE END OF JANUARY, 1984.

1/84 SYSTEM 744

KANSAS CITY POWER & LIGHT: LA CYGNE 1 (CONT.)

	PERFORMANCE DATA												
PERIOD						N % REMOVAL SO2 PART. H		PER			CAP.		
						202	PARI.	100K3					
2/84	SYSTEM							696					
3/84	SYSTEM							744					
4/84	SYSTEM							720					
5/84	SYSTEM							744					
6/84	SYSTEM							720					
7/84	SYSTEM							744					
8/84	SYSTEM							744					
9/84	SYSTEM							720					

^{**} PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED NO MAJOR FGD-RELATED OUTAGES DURING THE FIRST THREE QUARTERS OF 1984. FGD SYSTEM AVAILABILITY WAS ESTIMATED AT 95%.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COMPANY NAME	KANSAS POWER 8	LIGHT
PLANT NAME	JEFFREY	
UNIT NUMBER	1	
CITY	WAMEGO	
STATE	KANSAS	
REGULATORY CLASSIFICATION	C	
PARTICULATE EMISSION LIMITATION - NG/J		(.100 LB/MMBTU)
SO2 EMISSION LIMITATION - NG/J	322.	(.750 LB/MMBTU)
NOX EMISSION LIMITATION - NG/J	****	(***** LB/MMBTU)
NET PLANT GENERATING CAPACITY - MW	2720	
GROSS UNIT GENERATING CAPACITY - MW	720	
NET UNIT GENERATING CAPACITY W/FGD - MW	680	
NET UNIT GENERATING CAPACITY WO/FGD - MW EQUIVALENT SCRUBBED CAPACITY - MW	495 540	
EGOTAMENT SCHOODER CAPACITY & IM	540	
** UNIT DATA - BOILER AND STACK		
BOILER SUPPLIER	COMBUSTION ENG	THEEDTHO
BOILER TYPE	PULVERIZED COA	
BOILER SERVICE LOAD	BASE	· L
DESIGN BOILER FLUE GAS FLOW - CU.M/S		(2781000 ACFM)
BOILER FLUE GAS TEMPERATURE - C		
STACK HEIGHT - M	135.6 183.	(600 FT)
STACK SHELL	CONCRETE	(800 FT)
STACK TOP DIAMETER - M	7 0	(26.0 FT)
STACK TOP BIANCIER - II	7.7	(20.0 F1)
** FUEL DATA		
FUEL TYPE	COAL	
FUEL GRADE	SUBBITUMINOUS	
AVERAGE HEAT CONTENT - J/G		(8125 BTU/LB)
RANGE HEAT CONTENT - BTU/LB	200777	*****
AVERAGE ASH CONTENT - %	5.8 0	
RANGE ASH CONTENT - %	****	
AVERAGE MOISTURE CONTENT - X	30.00	
RANGE MOISTURE CONTENT + %	****	
AVERAGE SULFUR CONTENT - %	.32	
RANGE SULFUR CONTENT - %	*****	
AVERAGE CHLORIDE CONTENT - %	.01	
RANGE CHLORIDE CONTENT - %	*****	
*** PARTICLE CONTROL		
** MECHANICAL COLLECTOR		
NUMBER	0	
TYPE	NONE	
** ESP		
NUMBER	2	
TYPE	COLD SIDE	
SUPPLIER	C.E. WALTHER	
INLET FLUE GAS CAPACITY - CU.M/S	664.0	(1407000 ACFM)
INLET FLUE GAS TEMPERATURE - C	160.0	(320 F)
PRESSURE DROP - KPA	. 3	(1. IN-H2O)
PARTICLE REMOVAL EFFICENCY - %	98.6	
XX DARTICLE COMPACE		
** PARTICLE SCRUBBER	_	
NUMBER CENERAC TYPE	0	
GENERIC TYPE	NONE	
SPECIFIC TYPE	N/A	
TRADE NAME/COMMON NAME	N/A	
SHELL GENERIC MATERIAL	N/A	
SHELL SPECIFIC MATERIAL	H/A	
LINER GENERIC MATERIAL	N/A	
LINER SPECIFIC MATERIAL GAS CONTACTING DEVICE TYPE	N/A	
GAS CONTACTING DEVICE TYPE	N/A	
*** FGD SYSTEM		
····· (OD 31316))		

KANSAS POWER & LIGHT: JEFFREY 1 (CONT.)

```
** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                               THROWAWAY PRODUCT
   SO2 REMOVAL MODE
                                               WET SCRUBBING
                                                LIMESTONE
   PROCESS TYPE
   PROCESS ADDITIVES
                                               NONE
   SYSTEM SUPPLIER
                                                COMBUSTION ENGINEERING
                                                BLACK & VEATCH
   A-E FIRM
   DEVELOPMENT LEVEL
                                                FULL SCALE
   NEW/RETROFIT
                                               NEW
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - %
                                                  99.00
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                   60.00
   CURRENT STATUS
   COMMERCIAL START-UP
                                                 8/78
   INITIAL START-UP
                                                 8/78
   CONTRACT AWARDED
                                                 7/73
** DESIGN AND OPERATING PARAMETERS
** QUENCHER/PRESATURATOR
   NUMBER
                                                 Û
** ABSORBER
   NUMBER
                                                 6
   NUMBER OF SPARES
                                                 1
                                                SPRAY TOWER
   GENERIC TYPE
    SPECIFIC TYPE
                                                OPEN COUNTERCURRENT SPRAY
    TRADE NAME/COMMON TYPE
                                                N/A
    SUPPLIER
                                                COMBUSTION ENGINEERING
    SHELL GENERIC MATERIAL
                                                STAINLESS STEEL
    SHELL SPECIFIC MATERIAL
                                                AUSTENITIC
                                                TYPE 316L
    SHELL MATERIAL TRADE NAME/COMMON TYPE
    LINER GENERIC MATERIAL
                                                NONE
    LINER SPECIFIC MATERIAL
                                                N/A
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                                N/A
    GAS CONTACTING DEVICE TYPE
                                                NONE
   NUMBER OF CONTACTING ZONES
                                                 2
    LIQUID RECIRCULATION RATE - LITER/S
                                                  907.
                                                               (14400 GPM)
                                                               ( 39.7 GAL/1000 ACF)
    L/G RATIO - L/CU.M
                                                    5.3
    GAS-SIDE PRESSURE DROP - KPA
                                                    1.0
                                                               ( 4.0 IN-H20)
    INLET GAS FLOW - CU. M/S
                                                  171.30
                                                               ( 363000 ACFM)
                                                                  276 F)
    INLET GAS TEMPERATURE - C
                                                  135.6
    SO2 REMOVAL EFFICIENCY - %
                                                   60.0
** MIST ELIMINATOR
                                                PRECOLLECTOR
   PRE-MIST ELIMINATOR/MIST ELIMINATOR
    NUMBER PER SYSTEM
                                                 6
    NUMBER OF SPARES PER SYSTEM
                                                 1
   NUMBER PER MODULE
                                                 1
   GENERIC TYPE
                                                BULK SEPARATION
   SPECIFIC TYPE
                                                BAFFLE SLATS
   TRADE NAME/COMMON TYPE
                                                BULK ENTRAINMENT SEPARATOR
   CONFIGURATION
                                                HORIZONTAL
   NUMBER OF STAGES
                                                    1
   NUMBER OF PASSES PER STAGE
                                                    1
   CONSTRUCTION MATERIAL GENERIC TYPE
                                                ORGANIC
                                                FIBER-REINFORCED POLYESTER
   CONSTRUCTION MATERIAL SPECIFIC TYPE
   WASH WATER SOURCE
                                                NR
** REHEATER
   NUMBER
                                                 1
                                                BYPASS
   GENERIC TYPE
   SPECIFIC TYPE
                                                COLD SIDE
   TRADE NAME/COMMON TYPE
                                                N/A
   PERCENT GAS BYPASSED - AVG
                                                   25.0
                                                   27.8
                                                                   50 F)
   TEMPERATURE INCREASE - C
                                                               (
                                                               ( 120 F)
   INLET FLUE GAS TEMPERATURE - C
                                                   48.9
   OUTLET FLUE GAS TEMPERATURE - C
                                                               ( 170 F)
                                                   76.7
   CONSTRUCTION MATERIAL GENERIC TYPE
                                                NR
                                                NR
   CONSTRUCTION MATERIAL SPECIFIC TYPE
```

KANSAS POWER & LIGHT: JEFFREY 1 (CONT.)

** FANS

NUMBER
NUMBER OF SPARES
DESIGN
SUPPLIER
FUNCTION
APPLICATION
SERVICE
FLUE GAS TEMPERATURE - C
CONSTRUCTION MATERIAL GENERIC TYPE

FORCED DRAFT DRY 135.6 (276 F)

** DAMPERS

FUNCTION
GENERIC TYPE
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

SHUT-OFF LOUVER CARBON STEEL AISI 1110 NONE N/A

4

1

UNIT

CENTRIFUGAL

CARBON STEEL

GREEN FAN

** DAMPERS

FUNCTION
GENERIC TYPE
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

SHUT-OFF LOUVER CARBON STEEL AISI 1110 NONE N/A

** DAMPERS

FUNCTION
GENERIC TYPE
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

NR LOUVER CARBON STEEL AISI 1110 NONE N/A

** DUCTWORK

LOCATION
CONFIGURATION
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

ABSORBER INLET RECTANGULAR CARBON STEEL AISI 1110 NONE N/A

** DUCTWORK

LOCATION
CONFIGURATION
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

ABSORBER OUTLET TO REHEAT ZONE RECTANGULAR CARBON STEEL AISI 1110 ORGANIC COAL TAR EPOXY

** DUCTWORK
LOCATION

CONFIGURATION
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

REHEAT ZONE TO STACK
RECTANGULAR
CARBON STEEL
AISI 1110
INORGANIC
CHEMICALLY-BONDED CONCRETE

** DUCTWORK

CONFIGURATION
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

BYPASS RECTANGULAR CARBON STEEL AISI 1110 NONE N/A

** REAGENT PREPARATION EQUIPMENT FUNCTION

DEVICE

WET BALL MILL COMPARTMENTED

KANSAS POWER & LIGHT: JEFFREY 1 (CONT.)

NR DEVICE TYPE NUMBER

10.9 FULL LOAD DRY FEED CAPACITY - M.TONS/HR (12 TPH) 60.0

PRODUCT QUALITY - % SOLIDS

** TANKS

NUMBER SERVICE _____ -----ABSORBER RECYCLE 4 SLUDGE STORAGE *** SLUDGE TRANSFER **** MIST ELIMINATOR WASH ***

** PUMPS

SERVICE NUMBER ~~~~ ABSORBER RECIRCULATION 6 ABSORBER BLEED **** *** SLUDGE POND RETURN *** ADDITIVE FEED 4 ADDITIVE TRANSFER 3

** SOLIDS CONCENTRATING/DEWATERING

NONE DEVICE

*** SLUDGE

** TREATMENT

FORCED OXIDATION METHOD DEVICE AIR SPARGERS IN REACTION TANK PROPRIETARY PROCESS N/A

** DISPOSAL

FINAL NATURE TYPE POND LOCATION ON-SITE SITE TRANSPORTATION METHOD PIPELINE SITE TREATMENT CLAY LINING SITE DIMENSIONS 230 ACRES/80 FT SITE SERVICE LIFE - YRS 30

** PROCESS CONTROL AND INSTRUMENTATION

CHEMICAL PARAMETERS S02

MONITOR TYPE DUPONT & LEAR SIEGLER

** WATER BALANCE WATER LOOP TYPE

CLOSED MAKEUP WATER ADDITION - LITERS/S (577 GPM) 36.4

** CHEMICALS AND CONSUMPTION

FUNCTION **ABSORBENT** NAME LIMESTONE CONSUMPTION 12130 LB/HR POINT OF ADDITION BALL MILL

** FGD SPARE CAPACITY INDICES

ABSORBER - % 20.0

** FGD SPARE COMPONENT INDICES

ABSORBER 1.0

KANSAS POWER & LIGHT: JEFFREY 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

8/78 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER AND TURBINE WERE SYNCHRONIZED ON JUNE 11 AND THE BOILER IS NOW OPERATIONAL.

THE FGD SYSTEM IS IN THE SHAKEDOWN PHASE OF OPERATION. EACH OF THE SIX MODULES OPERATED DURING THIS PERIOD. NO MAJOR PROBLEMS WERE REPORTED. INTEGRATED OPERATION OF THE SYSTEM IS EXPECTED DURING THE FIRST HALF OF OCTOBER.

 9/78
 SYSTEM
 720

 10/78
 SYSTEM
 744

 11/78
 SYSTEM
 720

 12/78
 SYSTEM
 744

** PROBLEMS/SOLUTIONS/COMMENTS

INTEGRATED OPERATION FOR THIS UNIT HAS NOT YET BEEN ACHIEVED. A CERTIFICATION TEST WHICH HAD BEEN SCHEDULED WAS CANCELLED DUE TO A BOILER OUTAGE. AT THIS TIME THE COLD WEATHER HAS FORCED POSTPONMENT OF THE TEST INDEFINITELY. INTERMITTENT FGD OPERATIONS ARE CONTINUING.

 1/79
 SYSTEM
 744

 2/79
 SYSTEM
 672

 3/79
 SYSTEM
 744

** PROBLEMS/SOLUTIONS/COMMENTS

NO BOILER OR FGD SYSTEM PROBLEMS WERE REPORTED FOR FEBRUARY OR MARCH.

4/79 SYSTEM .0 720 0 0 .0 5/79 SYSTEM .0 744 0 0 .0

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER WAS SHUT DOWN FOR WARRANTY INSPECTION ON APRIL 1 AND REMAINED OUT OF SERVICE DURING MAY.

6/79 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE UNIT RETURNED TO SERVICE THE FIRST WEEK OF JUNE AND HAS SUFFERED NO OPERATIONAL DIFFICULTIES SINCE RESTART.

7/79 SYSTEM 744 8/79 SYSTEM 744 9/79 SYSTEM 720 KANSAS POWER & LIGHT: JEFFREY 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

NO UNUSUAL BOILER OR FGD SYSTEM PROBLEMS WERE ENCOUNTERED DURING JULY OR AUGUST. THE UNIT PASSED THE COMPLIANCE TEST DURING THE JUNE-JULY PERIOD. THE UNIT WILL SHUT DOWN IN MID-SEPTEMBER FOR THE NORMAL TWO WEEK INSPECTION AND MAINTENANCE OUTAGE. THE UNIT IS EXPECTED BACK ON LINE ON OCTOBER 1.

10/79 SYSTEM 744 11/79 SYSTEM 720 12/79 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY HAS REPORTED THAT THERE HAS BEEN NO MAJOR OPERATING PROBLEMS DURING THIS REPORT PERIOD. EXCESSIVE BALL WEAR IN THE LIMESTONE BALL MILL WAS DETECTED.

AGITATOR FAILURES IN THE REACTION TANK HAVE OCCURRED. THE AGITATORS HAVE EXPERIENCED MOTOR FAILURES, PADDLE ARM DETACHMENTS AND SHAFT BREAKING.

 1/80
 SYSTEM
 744

 2/80
 SYSTEM
 696

 3/80
 SYSTEM
 100.0
 100.0
 67.7
 744
 504
 504

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER WENT OFF LINE FOR TEN DAYS IN MARCH FOR A SCHEDULED INSPECTION. DURING THE BOILER OUTAGE GENERAL MAINTENANCE WAS PERFORMED ON THE FGD SYSTEM. OTHER THAN THIS OUTAGE, THE FGD UNIT OPERATED 100% OF THE TIME IN MARCH.

4/80	SYSTEM	100.0	100.0	100.0	100.0	720	720	720
5/80	SYSTEM	100.0	100.0	100.0	100.0	744	744	744
6/80	SYSTEM	100.0	100.0	100.0	100.0	720	720	720

** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE APRIL THROUGH JUNE PERIOD THE FGD SYSTEM OPERATED 100% OF THE TIME.

7/80 SYSTEM 100.0 100.0 100.0 69.1 744 514 514 49.3

** PROBLEMS/SOLUTIONS/COMMENTS

DURING JULY A 230 HOUR OUTAGE OCCURRED DUE TO AN AIR PREHEATER TUBE LEAK IN THE BOILER. NO FGD-RELATED PROBLEMS OCCURRED DURING THE MONTH.

8/80 SYSTEM 100.0 100.0 100.0 84.8 744 631 631 42.8

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS TAKEN OUT OF SERVICE FOR PART OF AUGUST SO REPAIRS COULD BE CONDUCTED ON BOILER AIR PREHEATER TUBES.

9/80 SYSTEM 100.0 100.0 100.0 100.0 720 720 720 67.7

KANSAS POWER & LIGHT: JEFFREY 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

NO PROBLEMS WITH THE BOILER OR THE FGD SYSTEM WERE ENCOUNTERED DURING SEPTEMBER.

10/80 SYSTEM 100.0 100.0 100.0 37.4 744 278 278

** PROBLEMS/SOLUTIONS/COMMENTS

DURING OCTOBER THE BOILER DID NOT OPERATE FOR APPROXIMATELY 466 HOURS DUE TO A SCHEDULED INSPECTION.

11/80 SYSTEM 99.9 99.8 99.8 86.8 720 626 625

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER WAS OUT OF SERVICE APPROXIMATELY 94 HOURS DUE TO BOILER INSPECTION AND BEARING FAILURES.

THE FGD SYSTEM WAS DOWN APPROXIMATELY ONE HOUR DUE TO AN AUTOMATIC DAMPER MALFUNCTION.

12/80 SYSTEM 100.0 100.0 100.0 98.5 744 733 733

** PROBLEMS/SOLUTIONS/COMMENTS

DURING DECEMBER THE FGD SYSTEM WAS AVAILABLE 100%.

A BOILER OUTAGE DURING THE MONTH WAS DUE TO A AIR PREHEATER PROBLEM.

 1/81
 SYSTEM
 744

 2/81
 SYSTEM
 672

 3/81
 SYSTEM
 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS OPERATED VERY LITTLE DURING THE FIRST QUARTER OF 1981. THE UTILITY FIRED LOW SULFUR COAL DURING THE PERIOD.

DURING THE MONTH OF MARCH THE SYSTEM WAS DOWN FOR A PERIOD OF TWO WEEKS DUE TO A SCHEDULED MAINTENANCE OUTAGE.

 4/81
 SYSTEM
 720

 5/81
 SYSTEM
 744

 6/81
 SYSTEM
 720

 7/81
 SYSTEM
 744

 8/81
 SYSTEM
 744

 9/81
 SYSTEM
 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE JEFFREY 1 FGD SYSTEM OPERATED INTERMITTENTLY DURING THE SECOND AND THIRD QUARTERS OF 1981. FLUE GAS GENERATED FROM THE LOW SULFUR CONTENT COAL BURNED THROUGHOUT MUCH OF THE PERIOD DID NOT REQUIRE SCRUBBING.

10/81 SYSTEM 720

KANSAS POWER & LIGHT: JEFFREY 1 (CONT.)

PERIOD	MODULE /	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION				BOILER HOURS	FGD HOURS	CAP. FACTOR
11/81	SYSTEM							720			
12/81	SYSTEM							744			
	** PROB	LEMS/SOLUTION	NS/COMMENTS								
			HE UTILITY RE		NO FGD-RELAT	TED PRO	BLEMS	WERE !	ENCOUNT	ERED DU	JRING
1/82	SYSTEM							744			
2/82	SYSTEM							672			
3/82	SYSTEM							744			
	** PROBLEMS/SOLUTIONS/COMMENTS										
		TI	HE FIRST QUAR	RTER 1982.	NO FGD-RELAT SOMETIME DURI UTDOWN FOR A	ING THE	FIRS	T AND/	OR SECO	ID QUAR	RTER
4/82	SYSTEM							720			
5/82	SYSTEM							744			
6/82	SYSTEM							720			
	** PROB	LEMS/SOLUTION	NS/COMMENTS								

THE UTILITY REPORTED THAT NO FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE SECOND QUARTER 1982.

7/82	SYSTEM	744
8/82	SYSTEM	744
9/82	SYSTEM	720
10/82	SYSTEM	744
11/82	SYSTEM	720
12/82	SYSTEM	744
1/83	SYSTEM	744
2/83	SYSTEM	672
3/83	SYSTEM	744

** PROBLEMS/SOLUTIONS/COMMENTS

THE JEFFREY 1 AND 2 FGD SYSTEMS HAVE NOT BEEN OPERATED SINCE THE FALL OF 1982 WHILE THE FINAL INSTALLATION WORK WAS COMPLETED ON THE JEFFREY 3 FGD SYSTEM.

THE REACTION TANKS HAVE EXPERIENCED CORROSION RELATED TO FLEXING OF THE STEEL TANK BASES. THIS HAS BEEN EVIDENCED PARTICULARLY AROUND THE MIXERS. KP&L IS NOW PUTTING IN CONCRETE TANK FLOORS TO ELIMINATE THE PROBLEM.

THE JEFFREY 1 AND 2 FGD SYSTEMS HAVE BEEN SHOWING CORROSION IN THE DOWNSTREAM DUCTWORK PARTICULARLY IN THE REHEAT MIXING ZONE. THE PROBLEM HAS NOT YET BECOME SERIOUS.

KANSAS POWER & LIGHT: JEFFREY 1 (CONT.)

	· -			PERFORMA	NCE DATA						
PERIOD	MODULE	AVAILABILIT	Y OPERABILITY	RELIABILITY	UTILIZATION	% REM				FGD HOURS	CAP. FACTOR
		~	- ******								
4/83	SYSTEM	100.0			.0			720		0	
	** PROE	SLEMS/SOLUTI	ONS/COMMENTS								
			THE JEFFREY 1 JEFFREY 3 WAS		REMAINED DOWN	WHILE	FINAL	INST	LLATION	WORK	ON
5/83	SYSTEM	100.0			.0			744		0	
6/83	SYSTEM	100.0			.0			720		0	
7/83	SYSTEM	100.0			. 0			744		0	
8/83	SYSTEM	100.0			.0			744		0	

** PROBLEMS/SOLUTIONS/COMMENTS

100.0

9/83 SYSTEM

THE JEFFREY 1 FGD SYSTEM WAS REPORTED TO HAVE BEEN AVAILABLE DURING THE PERIOD OF MAY THROUGH SEPTEMBER. HOWEVER, DURING THIS TIME, THE FGD SYSTEM WAS ONLY OPERATED FOR 1 MONTH DUE TO A SUMMER PEAK LOAD PERION.

. 0

720

THE NEXT UNIT OUTAGE IS SCHEDULED FOR THE FIRST OF DECEMBER. DURING THIS OUTAGE, THE UTILITY PLANS TO DO SOME PATCH WORK ON THE ABSORBER OUTLET DUCTING.

10/83	SYSTEM	744
11/83	SYSTEM	720
12/83	CYCTEM	744

** PROBLEMS/SOLUTIONS/COMMENTS

JEFFREY 1 WAS OUT OF SERVICE DURING THE FOURTH QUARTER OF 1983 DUE TO EXTENSIVE DUCTWORK REPAIRS.

1/84	SYSTEM	744
2/84	SYSTEM	696
3/84	SYSTEM	744
4/84	SYSTEM	720
5/84	SYSTEM	744
6/84	SYSTEM	720
7/84	SYSTEM	744
8/84	SYSTEM	744
9/84	SYSTEM	720

** PROBLEMS/SOLUTIONS/COMMENTS

JEFFREY 1 WAS OFF LINE DURING 1984. THE UTILITY REPORTED THAT THE REPLACEMENT OF CORRODING OUTLET DUCTWORK IS PLANNED FOR THE NEXT SIX MONTHS.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

		• * * * * * * * * * * * * * * * * * * *
THE PARTY WAR	MANICAC DOMED 4	TCHT
COMPANY NAME	KANSAS POWER &	LIGHT
PLANT NAME	JEFFREY	
UNIT NUMBER	2	
CITY	WAMEGO	
STATE	KANSAS	
REGULATORY CLASSIFICATION	С	
PARTICULATE EMISSION LIMITATION - NG/J	43.	(.100 LB/MMBTU)
SO2 EMISSION LIMITATION - NG/J	322.	(.750 LB/MMBTU)
NOX EMISSION LIMITATION - NG/J		(***** LB/MMBTU)
NET PLANT GENERATING CAPACITY - MW	2720	(AAAAA LD/IIIDIO)
GROSS UNIT GENERATING CAPACITY - MW	720	
NET UNIT GENERATING CAPACITY W/FGD - MW	680	
NET UNIT GENERATING CAPACITY WO/FGD - MW	495	
EQUIVALENT SCRUBBED CAPACITY - MW	540	
** UNIT DATA - BOILER AND STACK		
BOILER SUPPLIER	COMBUSTION ENG	STNEERING
BOILER TYPE	PULVERIZED COA	
BOILER SERVICE LOAD		` `
	BASE	/ A 7 A 4 A 4 A 7 M 1
DESIGN BOILER FLUE GAS FLOW - CU.M/S	1312.35	(2781000 ACFM)
BOILER FLUE GAS TEMPERATURE - C		(276 F)
STACK HEIGHT - M	183.	(600·FT)
STACK SHELL	CONCRETE	
STACK TOP DIAMETER - M	7.9	(26.0 FT)
** FUEL DATA		
FUEL TYPE	COAL	
FUEL GRADE	SUBBITUMINOUS	
AVERAGE HEAT CONTENT - J/G		(010E DTI/ID)
	18899.	(8125 BTU/LB)
RANGE HEAT CONTENT - BTU/LB		*****
AVERAGE ASH CONTENT - %	5.80	
RANGE ASH CONTENT - %	****	
AVERAGE MOISTURE CONTENT - %	30.00	
RANGE MOISTURE CONTENT - %	*****	
AVERAGE SULFUR CONTENT - %	.32	
RANGE SULFUR CONTENT - %	*****	
AVERAGE CHLORIDE CONTENT - %	.01	
RANGE CHLORIDE CONTENT - %	*****	
RANGE CHECKIDE CONTENT - 7.	*****	
XXX DADITOLE CONTDOL		
*** PARTICLE CONTROL		
VV MEANINE AND ADDRESS OF THE PARTY OF THE P		
** MECHANICAL COLLECTOR	_	
NUMBER	0	
TYPE	NONE	
** ESP		
NUMBER	2	
TYPE	COLD SIDE	
SUPPLIER	C.E. WALTHER	
INLET FLUE GAS CAPACITY - CU.M/S	664.0	(1407000 ACFM)
INLET FLUE GAS TEMPERATURE - C	160.0	(320 F)
PRESSURE DROP - KPA	.3	(1. IN-H2O)
PARTICLE REMOVAL EFFICENCY - %	98.6	
** PARTICLE SCRUBBER	_	
NUMBER	0	
GENERIC TYPE	NONE	
SPECIFIC TYPE	N/A	
TRADE NAME/COMMON NAME	N/A	
SHELL GENERIC MATERIAL	N/A	
SHELL SPECIFIC MATERIAL	N/A	
	N/A	
LINER GENERIC MATERIAL		
LINER SPECIFIC MATERIAL	N/A	
GAS CONTACTING DEVICE TYPE	N/A	

*** FGD SYSTEM

KANSAS POWER & LIGHT: JEFFREY 2 (CONT.)

```
** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                              THROWAWAY PRODUCT
   SO2 REMOVAL MODE
                                              WET SCRUBBING
                                               LIMESTONE
   PROCESS TYPE
   SYSTEM SUPPLIER
                                               COMBUSTION ENGINEERING
                                               BLACK & VEATCH
   A-E FIRM
   DEVELOPMENT LEVEL
                                               FULL SCALE
                                              NEW
   NEW/RETROETT
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.00
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - X
                                                 60.00
   CURRENT STATUS
                                               1
   COMMERCIAL START-UP
                                               5/80
   INITIAL START-UP
                                               1/80
   CONTRACT AWARDED
                                               7/73
** DESIGN AND OPERATING PARAMETERS
** QUENCHER/PRESATURATOR
   NUMBER
                                               0
** ABSORBER
   NUMBER
                                               6
   NUMBER OF SPARES
   GENERIC TYPE
                                              SPRAY TOWER
   SPECIFIC TYPE
                                              OPEN COUNTERCURRENT SPRAY
    TRADE NAME/COMMON TYPE
                                              N/A
   SUPPLIER
                                              COMBUSTION ENGINEERING
   SHELL GENERIC MATERIAL
                                              STAINLESS STEEL
   SHELL SPECIFIC MATERIAL
                                              AUSTENITIC
   SHELL MATERIAL TRADE NAME/COMMON TYPE
                                              TYPE 316L
   LINER GENERIC MATERIAL
                                              NONE
   LINER SPECIFIC MATERIAL
                                              N/A
   LINER MATERIAL TRADE NAME/COMMON TYPE
                                              N/A
   GAS CONTACTING DEVICE TYPE
                                              NONE
   NUMBER OF CONTACTING ZONES
   LIQUID RECIRCULATION RATE - LITER/S
                                                907.
                                                             (14400 GPM)
   L/G RATIO - L/CU.M
                                                5.3
                                                             ( 39.7 GAL/1000 ACF)
   GAS-SIDE PRESSURE DROP - KPA
                                                  1.0
                                                             ( 4.0 IN-H20)
   INLET GAS FLOW CU. M/S
                                                171.30
                                                             ( 363000 ACFM)
   INLET GAS TEMPERATURE - C
                                                135.6
                                                             ( 276 F)
   SO2 REMOVAL EFFICIENCY - X
                                                 60.0
** MIST FLIMINATOR
   PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                              PRECOLLECTOR
   NUMBER PER SYSTEM
                                               6
   NUMBER OF SPARES PER SYSTEM
                                               1
   NUMBER PER MODULE
   GENERIC TYPE
                                              BULK SEPARATION
   SPECIFIC TYPE
                                              BAFFLE SLATS
   TRADE NAME/COMMON TYPE
                                              BULK ENTRAINMENT SEPARATOR
   CONFIGURATION
                                              HORIZONTAL
   NUMBER OF STAGES
                                                  1
   NUMBER OF PASSES PER STAGE
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              ORGANIC
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              FIBER-REINFORCED POLYESTER
   WASH WATER SOURCE
                                              ИÐ
** REHEATER
   NUMBER
                                               1
   GENERIC TYPE
                                              BYPASS
   SPECIFIC TYPE
                                              COLD SIDE
   TRADE NAME/COMMON TYPE
                                              N/A
   PERCENT GAS BYPASSED - AVG
                                               25.0
   TEMPERATURE INCREASE - C
                                                 27.8
                                                             ( 50 F)
   INLET FLUE GAS TEMPERATURE - C
                                                 48.9
                                                            ( 120 F)
   OUTLET FLUE GAS TEMPERATURE - C
                                                 76.7
                                                            ( 170 F)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              NR
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              NR
```

KANSAS POWER & LIGHT: JEFFREY 2 (CONT.)

** FANS

NUMBER NUMBER OF SPARES

DESIGN SUPPLIER **FUNCTION** APPLICATION SERVICE

FLUE GAS TEMPERATURE - C

CONSTRUCTION MATERIAL GENERIC TYPE

** DAMPERS

FUNCTION GENERIC TYPE CONSTRUCTION MATERIAL GENERIC TYPE

CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE

LINER SPECIFIC MATERIAL TYPE

** DAMPERS

FUNCTION GENERIC TYPE CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE

LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE

** DAMPERS

FUNCTION GENERIC TYPE

CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE

LINER SPECIFIC MATERIAL TYPE

** DUCTWORK

LOCATION CONFIGURATION

SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE

** DUCTWORK

LOCATION CONFIGURATION

SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GEMERIC MATERIAL TYPE

LINER SPECIFIC MATERIAL TYPE

** DUCTWORK

LOCATION CONFIGURATION

SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE

LINER SPECIFIC MATERIAL TYPE

** DUCTWORK

LOCATION CONFIGURATION

SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE

** REAGENT PREPARATION EQUIPMENT

FUNCTION DEVICE

4 1

CENTRIFUGAL GREEN FAN UNIT

FORCED DRAFT

DRY

135.6 (276 F)

CARBON STEEL

SHUT-OFF LOUVER CARBON STEEL AISI 1110

NONE N/A

SHUT-OFF LOUVER CARBON STEEL AISI 1110

NONE N/A

NR LOUVER CARBON STEEL AISI 1110 NONE

ABSORBER INLET RECTANGULAR CARBON STEEL AISI 1110

NONE N/A

N/A

ABSORBER OUTLET TO REHEAT ZONE

RECTANGULAR CARBON STEEL AISI 1110 ORGANIC COAL TAR EPOXY

REHEAT ZONE TO STACK

RECTANGULAR CARBON STEEL AISI 1110 INORGANIC

CHEMICALLY-BONDED CONCRETE

BYPASS RECTANGULAR CARBON STEEL AISI 1110

NONE N/A

WET BALL MILL COMPARTMENTED

KANSAS POWER & LIGHT: JEFFREY 2 (CONT.)

DEVICE TYPE NR NUMBER

FULL LOAD DRY FEED CAPACITY - M.TONS/HR 10.9 (12 TPH)

PRODUCT QUALITY - % SOLIDS 60.0

** TANKS

SERVICE NUMBER

ABSORBER RECYCLE 4

SLUDGE STORAGE ****

SLUDGE TRANSFER ****

MIST ELIMINATOR WASH ****

** PUMPS

SERVICE NUMBER

ABSORBER RECIRCULATION 6
ABSORBER BLEED ****
SLUDGE ****
POND RETURN ****
ADDITIVE FEED 4
ADDITIVE TRANSFER 3

** SOLIDS CONCENTRATING/DEWATERING

DEVICE NONE

*** SLUDGE

** TREATMENT
METHOD FORCED OXIDATION

DEVICE AIR SPARGERS IN REACTION TANK

PROPRIETARY PROCESS N/A

** DISPOSAL NATURE

NATURE FINAL
TYPE POND
LOCATION ON-SITE
SITE TRANSPORTATION METHOD PIPELINE
SITE TREATMENT CLAY LINING
SITE DIMENSIONS 230 ACRES/80 FT
SITE SERVICE LIFE - YRS 30

** PROCESS CONTROL AND INSTRUMENTATION

CHEMICAL PARAMETERS SO2

MONITOR TYPE DUPONT & LEAR SIEGLER

** WATER BALANCE

WATER LOOP TYPE CLOSED

MAKEUP WATER ADDITION - LITERS/S 36.4 (577 GPM)

** CHEMICALS AND CONSUMPTION

FUNCTION ABSORBENT
NAME LIMESTONE
CONSUMPTION 12130 LB/HR
POINT OF ADDITION BALL MILL

** FGD SPARE CAPACITY INDICES

ABSORBER - % 20.0

** FGD SPARE COMPONENT INDICES

ABSCREER 1.0

			Y OPERABILITY F	RELIABILITY	UTILIZATION	% REM	10VAL	PER			
1/80	SYSTEM							744			
• • • •	SYSTEM							696			
	SYSTEM							744			
	** PROS	BLEMS/SOLUTI	ONS/COMMENTS								
			INITIAL OPERATI			IN JAN	UARY	1980.	LAM ON	OR PROE	LEMS
4/80	SYSTEM							720			
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS								
			DURING APRIL TH	HE SYSTEM W	AS STILL IN T	HE SHA	KEDOW	N/DEBU	GGING P	HASE OF	;
5/80	SYSTEM	100.0	100.0	100.0	100.0			744	744	744	
6/80	SYSTEM	100.0	100.0	100.0	100.0			720	720	720	
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS								
			COMMERCIAL OPER NO PROBLEMS ENC OF THE TIME.								
7/80	SYSTEM	100.0	100.0	100.0	95.3			744	709	709	81.0
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS								
			DURING JULY A I								AK
8/80	SYSTEM	100.0	100.0	100.0	100.0			744	744	744	80.1
9/80	SYSTEM	100.0	100.0	100.0	100.0			720	720	720	73.3
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS								
			NO PROBLEMS WER AUGUST AND SEP			BOILER	OR T	HE FGD	SYSTEM	DURING	THE
10/80	SYSTEM	100.0	100.0	100.0	100.0			744	744	744	
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS								
			THE UTILITY REP		NO MAJOR PRO	BLEMS	WERE	ENCOUN	TERED D	URING 1	THE
11/80	SYSTEM	100.0	100.0	100.0	56.1			720	404	404	
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS								
			DURING NOVEMBER ER WAS OUT OF								
12/80	SYSTEM	100.0	100.0	100.0	62.9			744	468	468	

KANSAS POWER & LIGHT: JEFFREY 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

DURING DECEMBER THE BOILER WAS OUT OF SERVICE DUE TO SUPERHEATER TUBE PROBLEMS. DURING THIS TIME THE FGD SYSTEM WAS 100% AVAILABLE.

1/81 SYSTEM 744 2/81 SYSTEM 672 3/81 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS NOT OPERATED MUCH DURING THE FIRST QUARTER OF 1981 BECAUSE THE UTILITY WAS ABLE TO MEET COMPLIANCE USING ONLY LOW SULFUR COAL.

THE UNIT WAS SHUT DOWN ALL OF MARCH AND PART OF FEBRUARY (SIX WEEKS) FOR AN EQUIPMENT WARRANTY INSPECTION.

 4/81
 SYSTEM
 720

 5/81
 SYSTEM
 744

 6/81
 SYSTEM
 720

 7/81
 SYSTEM
 744

 8/81
 SYSTEM
 744

 9/81
 SYSTEM
 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE JEFFREY 2 FGD SYSTEM OPERATED INTERMITTENTLY DURING THE SECOND AND THIRD QUARTERS OF 1981. FLUE GAS GENERATED FROM THE LOW SULFUR CONTENT COAL BURNED THROUGHOUT MUCH OF THE PERIOD DID NOT REQUIRE SCRUBBING.

 10/81
 SYSTEM
 744

 11/81
 SYSTEM
 720

 12/81
 SYSTEM
 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE FOURTH QUARTER.

 1/82
 SYSTEM
 744

 2/82
 SYSTEM
 672

 3/82
 SYSTEM
 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE FIRST QUARTER 1982. SOMETIME DURING THE FIRST AND/OR SECOND QUARTER 1982, THE UNIT WILL BE SHUTDOWN FOR A SCHEDULED 2 WEEK SPRING OUTAGE.

4/82 SYSTEM 720 5/82 SYSTEM 744 KANSAS POWER & LIGHT: JEFFREY 2 (CONT.)

	PERFORMANCE DATA										
PERIOD MO	DULE AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% REI	MOVAL	PER	BOILER	FGD	CAP.	
,					S02	PART.	HOURS	HOURS	HOURS	FACTOR	
6/82 SY	STEM						720				

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE SECOND QUARTER 1982.

7/82	SYSTEM	744
8/82	SYSTEM	744
9/82	SYSTEM	720
10/82	SYSTEM	744
11/82	SYSTEM	720
12/82	SYSTEM	744
1/83	SYSTEM	744
2/83	SYSTEM	672
3/83	SYSTEM	744

** PROBLEMS/SOLUTIONS/COMMENTS

THE JEFFREY 1 AND 2 FGD SYSTEMS HAVE NOT BEEN OPERATED SINCE THE FALL OF 1982 WHILE THE FINAL INSTALLATION WORK WAS COMPLETED ON THE JEFFREY 3 FGD SYSTEM.

THE REACTION TANKS HAVE EXPERIENCED CORROSION RELATED TO FLEXING OF THE STEEL TANK BASES. THIS HAS BEEN EVIDENCED PARTICULARLY AROUND THE MIXERS. KP&L IS NOW PUTTING IN CONCRETE TANK FLOORS TO ELIMINATE THE PROBLEM.

THE JEFFREY 1 AND 2 FGD SYSTEMS HAVE BEEN SHOWING CORROSION IN THE DOWNSTREAM DUCTWORK PARTICULARLY IN THE REHEAT MIXING ZONE. THE PROBLEM HAS NOT YET BECOME SERIOUS.

4/83 SYSTEM	100.0	.0	720	0
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** PROBLEMS/SOLUTIONS/COMMENTS

THE JEFFREY 2 FGD SYSTEM REMAINED DOWN WHILE FINAL INSTALLATION WORK ON JEFFREY 3 WAS COMPLETED.

5/83	SYSTEM	100.0	.0	744	0
6/83	SYSTEM	100.0	.0	720	0
7/83	SYSTEM	100.0	.0	744	0
8/83	SYSTEM	100.0	.0	744	0
9/83	SYSTEM	100.0	.0	720	0

** FROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT ALTHOUGH THE FGD SYSTEM WAS AVAILABLE THROUGHOUT THE PERIOD BETWEEN MAY AND SEPTEMBER, THE SYSTEM WAS NOT REQUIRED TO OPERATE.

THE NEXT UNIT OUTAGE IS SCHEDULED FOR NOVEMBER. DURING THIS OUTAGE, THE

KANSAS POHER & LIGHT: JEFFREY 2 (CONT.)

# @ # # # # # # # # # # # # # # # # # #	PERFORMANCE DATA	
PERIOD MODULE AVAILABILITY OPERABILITY	··· · - · · · · · · · · · · · · · · · · · ·	PER BOILER FGD CAP. HOURS HOURS HOURS FACTOR
UTILITY PLANS	TO DO SOME PATCH WORK ON THE ABSORBE	R OUTLET DUCTING.
10/83 SYSTEM		744
11/83 SYSTEM		720
12/83 SYSTEM		744

** PROBLEMS/SOLUTIONS/COMMENTS

JEFFREY 2 WAS OUT OF SERVICE DURING THE FOURTH QUARTER OF 1983, HOWEVER THE FGD SYSTEM WAS CONSIDERED 100% AVAILABLE.

1/84	SYSTEM	744
2/84	SYSTEM	696
3/84	SYSTEM	744
4/84	SYSTEM	720
5/84	SYSTEM	744
6/84	SYSTEM	720
7/84	SYSTEM	744
8/84	SYSTEM	744
9/84	SYSTEM	720

** PROBLEMS/SOLUTIONS/COMMENTS

OVERALL FGD SYSTEM AVAILABILITY FOR THE FIRST THREE QUARTERS OF 1984 WAS ESTIMATED AT OVER 85%. NO MAOR FGD-RELATED PROBLEMS WERE REPORTED.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

		=======================================
COMPANY NAME	KANSAS POWER &	LIGHT
PLANT NAME	JEFFREY	
UNIT NUMBER	3	
CITY	WAMEGO	
STATE	KANSAS	
REGULATORY CLASSIFICATION	C	
PARTICULATE EMISSION LIMITATION - NG/J	43.	(.100 LB/MMBTU) (***** LB/MMBTU)
SO2 EMISSION LIMITATION - NG/J	43. *****	(**** LB/MMBTU)
MOX ENTOSTON FILLIALION - MONO	****	(***** LB/MMBTU)
NET PLANT GENERATING CAPACITY - MW	2720	
GROSS UNIT GENERATING CAPACITY - MW	730	
NET UNIT GENERATING CAPACITY W/FGD - MW	680	
NET UNIT GENERATING CAPACITY WO/FGD - MW	495	
EQUIVALENT SCRUBBED CAPACITY - MW	540	
** UNIT DATA - BOILER AND STACK		
BOILER SUPPLIER	COMBUSTION ENG	THEFPTHS
BOILER TYPE	PULVERIZED COA	
BOILER SERVICE LOAD	BASE	.•
DESIGN BOILER FLUE GAS FLOW - CU.M/S		(2781000 ACFM)
BOILER FLUE GAS TEMPERATURE - C	135.6	(2781000 ACFM) (276 F)
STACK HEIGHT - M		(600 FT)
STACK SHELL	CONCRETE	
STACK TOP DIAMETER - M		(26.0 FT)
** FUEL DATA		
FUEL TYPE	COAL	
FUEL GRADE	SUBBITUMINOUS	
AVERAGE HEAT CONTENT - J/G	18899.	(8125 BTU/LB)
RANGE HEAT CONTENT - BTU/LB		****
AVERAGE ASH CONTENT - %	5.80 *****	
RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - %		
RANGE MOISTURE CONTENT - %	30.00 *****	
AVERAGE SULFUR CONTENT - %	.32	
RANGE SULFUR CONTENT - %	*****	
AVERAGE CHLORIDE CONTENT - %	.01	
RANGE CHLORIDE CONTENT - %	*****	
*** PARTICLE CONTROL		
** MECHANICAL COLLECTOR		
NUMBER	0	
TYPE	NONE	
****	NO.	
** ESP		
NUMBER	2	
TYPE	COLD SIDE	
SUPPLIER	C.E. WALTHER	
INLET FLUE GAS CAPACITY - CU.M/S	664.0	(1407000 ACFM)
INLET FLUE GAS TEMPERATURE - C	160.0	(320 F)
PRESSURE DROP + KPA	.3	(1. IN-H2O)
PARTICLE REMOVAL EFFICENCY - %	98.6	
** PARTICLE SCRUBBER		
NUMBER	0	
GENERIC TYPE	NONE	
*** FGD SYSTEM		
** GENERAL DATA		
SALEABLE PRODUCT/THROHAWAY PRODUCT	THROWAWAY PROD	DUCT
SO2 REMOVAL MODE	WET SCRUESING	
PROCESS TYPE	LIMESTONE	
SYSTEM SUPPLIER	COMBUSTION ENG	
A-E FIRM	BLACK & VEATCH	1
DEVELOPMENT LEVEL	FULL SCALE	
NEH/RETROFIT	NEW	
UNIT DESIGN PARTICLE REMOVAL EFFICIENCY	- / 99.00	

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KANSAS POHER & LIGHT: JEFFREY 3 (CONT.)
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UNIT DESIGN SO2 REMOVAL EFFICIENCY ~ % 60.00
CURRENT STATUS 1
COMMERCIAL START-UP 5/83
INITIAL START-UP 5/83

** DESIGN AND OPERATING PARAMETERS

** ABSORBER NUMBER 4 GENERIC TYPE SPECIFIC TYPE TRADE NAME/COMMON TYPE N/A SUPPLIER SHELL GENERIC MATERIAL SHELL SPECIFIC MATERIAL SHELL MATERIAL TRADE NAME/COMMON TYPE LINER GENERIC MATERIAL NONE N/A LINER SPECIFIC MATERIAL LINER MATERIAL TRADE NAME/COMMON TYPE N/A GAS CONTACTING DEVICE TYPE NONE NUMBER OF CONTACTING ZONES 907. LIQUID RECIRCULATION RATE - LITER/S L/G RATIO - L/CU.M GAS-SIDE PRESSURE DROP - KPA INLET GAS FLOW - CU. M/S INLET GAS TEMPERATURE - C

** MIST ELIMINATOR

PRE-MIST ELIMINATOR/MIST ELIMINATOR

NUMBER PER SYSTEM

SO2 REMOVAL EFFICIENCY - %

NUMBER OF SPARES PER SYSTEM
NUMBER PER MODULE
GENERIC TYPE
SPECIFIC TYPE
TRADE NAME/COMMON TYPE
CONFIGURATION
NUMBER OF STAGES
NUMBER OF PASSES PER STAGE

CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE WASH WATER SOURCE

** REHEATER

NUMBER
GENERIC TYPE
SPECIFIC TYPE
TRADE NAME/COMMON TYPE
PERCENT GAS BYPASSED - AVG
TEMPERATURE INCREASE - C
INLET FLUE GAS TEMPERATURE - C
OUTLET FLUE GAS TEMPERATURE - C
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE

** FANS

NUMBER
NUMBER OF SPARES
DESIGN
SUPPLIER
FUNCTION
APPLICATION
SERVICE
FLUE GAS TEMPERATURE - C
CONSTRUCTION MATERIAL GENERIC TYPE

** DAMPERS

FUNCTION
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
LINER GENERIC MATERIAL TYPE

SPRAY TOWER OPEN COUNTERCURRENT SPRAY COMBUSTION ENGINEERING STAINLESS STEEL **AUSTENITIC** TYPE 316L (14400 GPM) 5.3 (39.7 GAL/1000 ACF) (4.0 IN-H20) 1.0 171.30 (363000 ACFM) 135.6 (276 F) 60.0

PRECOLLECTOR

6
1
1
BULK SEPARATION
BAFFLE SLATS
BULK ENTRAINMENT SEPARATOR
HORIZONTAL
1
ORGANIC
FIBER-RETNEORCED POLYESTER

FIBER-REINFORCED POLYESTER NR

1 BYPASS COLD SIDE N/A 25.0 27.8 (50 F) 48.9 (120 F) 76.7 (170 F)

NR NR

> 4 1 CENTRIFUGAL GREEN FAN UNIT

DRY 135.6 (276 F) CARBON STEEL

SHUT-OFF CARBON STEEL AISI 1110 NONE

FORCED DRAFT

KANSAS POWER & LIGHT: JEFFREY 3 (CONT.)

LINER SPECIFIC MATERIAL TYPE

N/A

** DAMPERS

FUNCTION CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE

SHUT-OFF CARBON STEEL AISI 1110 NONE N/A

** DAMPERS

FUNCTION CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE

NR CARBON STEEL AISI 1110 NONE NZA

** DUCTWORK

LOCATION CONFIGURATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE

ABSORBER INLET RECTANGULAR CARBON STEEL AISI 1110 NONE N/A

** DUCTWORK LOCATION

> CONFIGURATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE

ABSORBER OUTLET TO REHEAT ZONE RECTANGULAR CARBON STEEL AISI 1110 ORGANIC COAL TAR EPOXY

** DUCTWORK

LOCATION

CONFIGURATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE

REHEAT ZONE TO STACK RECTANGULAR CARBON STEEL AISI 1110 INORGANIC CHEMICALLY-BONDED MORTAR

** DUCTWORK LOCATION

> CONFIGURATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE

BYPASS RECTANGULAR CARBON STEEL AISI 1110 NONE N/A

** REAGENT PREPARATION EQUIPMENT FUNCTION

DEVICE DEVICE TYPE FULL LOAD DRY FEED CAPACITY - M.TONS/HR PRODUCT QUALITY - % SOLIDS

WET BALL MILL COMPARTMENTED NR (12 TPH) 10.9

** TANKS

SERVICE SLUDGE STORAGE SLUDGE TRANSFER MIST ELIMINATOR WASH **** ABSORBER RECYCLE

NUMBER **** ****

60.0

** PUMPS

SERVICE ABSORBER RECIRCULATION ABSORDER BLEED SLUDGE POND RETURN

NUMBER -----6 **** **** ****

KANSAS POWER & LIGHT: JEFFREY 3 (CONT.)

ADDITIVE FEED 4
ADDITIVE TRANSFER 3

** SOLIDS CONCENTRATING/DEWATERING

DEVICE

*** SLUDGE

** TREATMENT

METHOD FORCED OXIDATION

DEVICE AIR SPARGERS IN REACTION TANK

PROPRIETARY PROCESS N/A

** DISPOSAL

NATURE FINAL
TYPE POND
LOCATION ON-SITE
SITE TRANSPORTATION METHOD PIPELINE
SITE TREATMENT CLAY LINING
SITE DIMENSIONS 230 ACRES/80 FT
SITE SERVICE LIFE - YRS 30

** WATER BALANCE

WATER LOOP TYPE CLOSED

** CHEMICALS AND CONSUMPTION

FUNCTION ABSORBENT
NAME LIMESTONE
CONSUMPTION 12130LB/HR
POINT OF ADDITION BALL MILL

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

5/83 SYSTEM 744

6/83 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE JEFFREY 3 FGD SYSTEM COMMENCED OPERATION IN MAY AND IS CURRENTLY IN THE STARTUP PHASE OF OPERATION.

THE JEFFREY 3 FGD SYSTEM IS SIMILIAR TO UNITS 1 AND 2 EXCEPT THAT THE OUTLET FROM THE ABSORBERS FEED INTO A COMMON BYPASS DUCT (FOR CONTINUOUS REHEAT) WHICH THEN EXITS INTO THE STACK. UNITS 1 AND 2 HAVE MIXING CHAMBER SECTIONS WHICH IN THE PAST HAVE CAUSED CORROSION PROBLEMS.

7/83 SYSTEM 744

8/83 SYSTEM 744

9/83 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT SINCE START UP, AT LEAST THREE OF THE FOUR ABSORBER SPRAY TOWERS HAVE OPERATED FULL TIME.

A UNIT OUTAGE FOR UNIT 3 BEGAN ON SEPTEMBER 17 AND WAS SCHEDULED TO LAST TWO WEEKS. HOWEVER, DUE TO SOME UNEXPECTED TURBINE PROBLEMS, THE UNIT OUTAGE MAY NOW LAST THREE WEEKS.

10/83 SYSTEM 744

11/83 SYSTEM 720

				PERFORMAN	HCE DATA							
PERIOD	MODULE AVA	ILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% RE	MOVAL	PER	BOILER	FGD	CAP.	
						S02	PART.	HOURS	HOURS	HOURS	FACTOR	
12/83	SYSTEM							744				

** PROBLEMS/SOLUTIONS/COMMENTS

JEFFREY 3 WAS DOWN DURING PART OF DECEMBER DUE TO PROBLEMS BROUGHT ABOUT BY THE EXTREME COLD WEATHER CONDITIONS.

1/84	SYSTEM	744
2/84	SYSTEM	696
3/84	SYSTEM	744
4/84	SYSTEM	720
5/84	SYSTEM	744
6/84		
	SYSTEM	720
7/84	SYSTEM	744
8/84	SYSTEM	744
9/84	SYSTEM	720

** PROBLEMS/SOLUTIONS/COMMENTS

OVERALL FGD SYSTEM AVAILABILITY FOR THE FIRST THREE QUARTERS OF 1984 WAS ESTIMATED AT OVER 85%. NO MAJOR FGD-RELATED PROBLEMS WERE REPORTED.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

KANSAS POWER & LIGHT COMPANY NAME LAWRENCE PLANT NAME UNIT NUMBER LAWRENCE CITY KANSAS STATE REGULATORY CLASSIFICATION PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW 576 125 GROSS UNIT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW 125
NET UNIT GENERATING CAPACITY W/FGD - MW 115
NET UNIT GENERATING CAPACITY WO/FGD - MW 495 495 125 EQUIVALENT SCRUBBED CAPACITY - MW ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER COMBUSTION ENGINEERING BOILER TYPE PULVERIZED COAL BOILER SERVICE LOAD CYCLING BOILER SERVICE LOAD

DESIGN BOILER FLUE GAS FLOW - CU.M/S

BOILER FLUE GAS TEMPERATURE - C

STACK HEIGHT M

STACK SHELL

CARBON STEEL (8.0 FT) STACK TOP DIAMETER - M 2.4 ** FUEL DATA FUEL TYPE COAL FUEL GRADE **** 23260. (10000 BTU/LB) AVERAGE HEAT CONTENT - J/G RANGE HEAT CONTENT - BTU/LB 9.80 **** AVERAGE ASH CONTENT - % 9.8-16 RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - % 11.80 RANGE MOISTURE CONTENT - % .55 0.55-0.90 AVERAGE SULFUR CONTENT - % RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - % *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER TYPE NONE ** ESP NUMBER TYPE NONE ** PARTICLE SCRUBBER NUMBER INITIAL START-UP DATE 1/76 GENERIC TYPE VENTURI TOWER SPECIFIC TYPE VARIABLE-THROAT/VERTICALLY-ADJUSTABLE ROD DECKS TRADE NAME/COMMON NAME ROD SCRUBBER SUPPLIER COMBUSTION ENGINEERING DIMENSIONS - FT 3.0 X 23.0 SHELL GENERIC MATERIAL STAINLESS STEEL SHELL SPECIFIC MATERIAL AUSTENITIC LINER GENERIC MATERIAL NONE LINER SPECIFIC MATERIAL N/A GAS CONTACTING DEVICE TYPE
NUMBER OF CONTACTING ZONES
LIQUID RECIRCULATION RATE - LITER/S NORYL-CLAD FRP RODS 1 226.8 LIGUID RECIRCULATION RATE - LITER/S 226.8 (3600 GPM)

L/G RATIO - LITER/CU.M 2.4 (17.9 GAL/1000ACF)

PRESSURE DROP - KPA 2.2 (9.0 IN-H20)

SUPERFICIAL GAS VELOCITY - M/S 15.2 (50.0 FT/S)

INLET GAS FLOW RATE CU.M/S 95.1 (201500 ACFM)

INLET GAS TEMPERATURE C 137.8 (280 F)

```
99.0
    PARTICLE REMOVAL EFFICIENCY - %
*** FGD SYSTEM
** GENERAL DATA
    SALEABLE PRODUCT/THROWAWAY PRODUCT
                                              THROWAWAY PRODUCT
                                              WET SCRUBBING
    SO2 REMOVAL MODE
                                              LIMESTONE
    PROCESS TYPE
    PROCESS ADDITIVES
                                              NONE
    SYSTEM SUPPLIER
                                              COMBUSTION ENGINEERING
    A-E FIRM
                                              BLACK & VEATCH
    DEVELOPMENT LEVEL
                                              FULL SCALE
    NEW/RETROFIT
                                              RETROFIT
    UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 98.90
    UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                73.00
    CURRENT STATUS
                                               1
    COMMERCIAL START-UP
                                               1/77
    INITIAL START-UP
                                               1/77
                                              12/68
    CONTRACT AHARDED
 ** DESIGN AND OPERATING PARAMETERS
 ** QUENCHER/PRESATURATOR
    NUMBER
                                               0
 ** ABSORBER
    NUMBER
                                              SPRAY TOHER
    GENERIC TYPE
    SPECIFIC TYPE
                                               OPEN COUNTERCURRENT SPRAY
    TRADE NAME/COMMON TYPE
                                              N/A
                                              COMBUSTION ENGINEERING
    SUPPLIER
    SHELL GENERIC MATERIAL
                                              STAINLESS STEEL
    SHELL SPECIFIC MATERIAL
                                               AUSTENITIC
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                              TYPE 316L
    LINER GENERIC MATERIAL
                                              NONE
    LINER SPECIFIC MATERIAL
                                              N/A
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                              N/A
    GAS CONTACTING DEVICE TYPE
                                              NONE
    NUMBER OF CONTACTING ZONES
                                              2
                                                         ( 5300 GPM)
( 30.4 GAL/1000 ACF)
( 2.5 IN-H20)
                                               334.
    LIQUID RECIRCULATION RATE - LITER/S
                                               4.1
    L/G RATIO - L/CU.M
                                                  .6
    GAS-SIDE PRESSURE DROP KPA
                                                 1.8
    SUPERFICAL GAS VELOCITY - M/SEC
                                                            ( 6.0 FT/S)
                                                82.35 ( 174500 ACFM)
    INLET GAS FLOW - CU. M/S
    INLET GAS TEMPERATURE C
                                                 51.1
                                                             ( 124 F)
    SO2 REMOVAL EFFICIENCY - %
                                                 73.0
 ** MIST ELIMINATOR
                                              PRIMARY COLLECTOR
    FRE-MIST ELIMINATOR/MIST ELIMINATOR
    NUMBER PER SYSTEM
                                               2
    NUMBER PER MODULE
                                               1
    GENERIC TYPE
                                              IMPINGEMENT
    SPECIFIC TYPE
                                              BAFFLE
                                               CLOSED VANE
    TRADE NAME/COMMON TYPE
    CONFIGURATION
                                              HORIZONTAL
    NUMBER OF STAGES
                                                   2
    NUMBER OF PASSES PER STAGE
                                                   2
    FREEBOARD DISTANCE - M
                                                   .09
                                                             ( .3 FT)
                                                30.48
                                                            (12.0 IN)
    DISTANCE BETHEEN STAGES - CM
    DISTANCE BETWEEN VANES CM
                                                  8.9
                                                            ( 3.50 IN)
                                                90
    VANE ANGLES - DEGREES
                                                   . 2
    PRESSURE DROP - KPA
                                                              ( 1.0 IN-H20)
    SUPERFICAL GAS VELOCITY - M/S
                                                  1.8
                                                             ( 6.0 FT/S)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                            ORGANIC
                                             FIBER-REINFORCED POLYESTER
    CONSTRUCTION MATERIAL SPECIFIC TYPE
    WASH WATER SOURCE
                                              POND RECYCLE
                                               ONCE/DAY
    WASH FREQUENCY
    WASH RATE - L/S
                                                 12.6
                                                           ( 200 GAL/MIN)
```

** REHEATER NUMBER NUMBER NUMBER PER MODULE GENERIC TYPE SPECIFIC TYPE TRADE NAME/COMMON TYPE PERCENT GAS BYPASSED - AVG TEMPERATURE INCREASE - C INLET FLUE GAS FLOW RATE - CU. M/S INLET FLUE GAS TEMPERATURE - C OUTLET FLUE GAS TEMPERATURE - C NUMBER OF HEAT EXCHANGER BANKS NUMBER OF TUBES PER BUNDLE CONSTRUCTION MATERIAL SPECIFIC TYPE	2 1 IN-LINE HOT WATER FIN TUBE .0 13.9 (25 F) 171.30 (363000 ACFM) 51.7 (125 F) 65.6 (150 F) 2 66 CARBON STEEL AISI 1110
** FANS NUMBER DESIGN SUPPLIER FUNCTION APPLICATION SERVICE FLUE GAS FLOW RATE - CU.M/S FLUE GAS TEMPERATURE C CONSTRUCTION MATERIAL GENERIC TYPE	2 CENTRIFUGAL BUFFALO FORGE BOOSTER INDUCED DRAFT DRY 80.22 (170000 ACFM) 62.8 (145 F) CARBON STEEL
** DAMPERS GENERIC TYPE SPECIFIC TYPE CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	LOUVER NR CARBON STEEL HIGH STRENGTH LOW ALLOY [HSLA] NONE N/A
** DAMPERS GENERIC TYPE SPECIFIC TYPE CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	LOUVER NR CARBON STEEL HIGH STRENGTH LOW ALLOY [HSLA] NONE N/A
** DAMPERS GENERIC TYPE SPECIFIC TYPE CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	LOUVER NR CARBON STEEL HIGH STRENGTH LOW ALLOY [HSLA] NONE N/A
** DUCTHORK LOCATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	SCRUBBER INLET CARBON STEEL HIGH STRENGTH LOW ALLOY [HSLA] NONE N/A
** DUCTWORK LOCATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	SCRUBBER OUTLET CARBON STEEL HIGH STRENGTH LOW ALLOY [HSLA] NONE N/A
** DUCTWORK LOCATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE	BYPASS CARBON STEEL HIGH STRENGTH LOW ALLOY [HSLA] NONE

LINER SPECIFIC MATERIAL TYPE N/A

** REAGENT PREPARATION EQUIPMENT

FUNCTION WET BALL MILL
DEVICE COMPARTMENTED
DEVICE TYPE NR
NUMBER 2

FULL LOAD DRY FEED CAPACITY - M.TONS/HR 5.4 (6 TPH)
PRODUCT QUALITY % SOLIDS 60.0

** TANKS

SERVICE NUMBER

ABSORBER RECYCLE 2
SCRUBBER RECYCLE 2
WASTE SLURRY BLEED 2
REAGENT PREP PRODUCT 1
MILL SUMP/PRODUCT ****
RECLAIMED WATER ****

** PUMPS

NUMBER SERVICE -----ADDITIVE FEED 6 MIST ELIMINATOR WASH **** VENTURI RECIRCULATION 2 ASSCRBER RECIRCULATION 2 MILL SLURRY ADDITIVE TRANSFER *** ADDITIVE STORAGE **** EFFLUENT BLEED **** THICKENER UNDERFLOW 2 MAKEUP WATER RECIRCULATION ****

** SOLIDS CONCENTRATING/DEWATERING

THICKENER DEVICE NUMBER 1 NUMBER OF SPARES 0 SHELL GENERIC MATERIAL TYPE CARBON STEEL HIGH STRENGTH LOW ALLOY [HSLA] SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A FEED STREAM SOURCE COLLECTION TANK FEED STREAM CHARACTERISTICS 8-10% SOLIDS OUTLET STREAM CHARACTERISTICS 30-35% SOLIDS TO POND OUTLET STREAM DISPOSITION

OVERFLOW STREAM DISPOSITION RECLAIMED WATER TANK

*** SLUDGE

** TREATMENT

METHOD FORCED OXIDATION
DEVICE REACTION TANK
PROPRIETARY PROCESS N/A
INLET QUALITY - % 10.0

** DISFOSAL

NATURE INTERIM
TYPE POND
LOCATION CN-SITE
SITE TRANSPORTATION METHOD PIPELINE
SITE TREATMENT NONE

** DISFOSAL

 NATURE
 FINAL

 TYPE
 POND

 LOCATION
 ON-SITE

SITE TRANSPORTATION METHOD OVERFLOW FROM INTERIM SLUDGE POND

SITE TREATMENT NONE

KANSAS POWER & LIGHT: LAWRENCE 4 (CONT.)

** PROCESS CONTROL AND INSTRUMENTATION

CHEMICAL PARAMETERS
PHYSICAL VARIABLES
CONTROL LEVELS
MONITOR LOCATION
PROCESS CONTROL MANNER
PROCESS CHEMISTRY MODE

PH, SO2 CONCENTRATION
PERCENT SOLIDS, SLURRY FLOW
PH 6.5
PH PROBES IN REACTION TANKS
AUTOMATIC

** WATER BALANCE WATER LOOP TYPE

CLOSED

FEEDBACK

** CHEMICALS AND CONSUMPTION

FUNCTION
NAME
PRINCIPAL CONSTITUENT
CONSUMPTION
POINT OF ADDITION

ABSORBENT LIMESTONE 93% CACO3, 7% MGCO3 1.5 TPH BALL MILL

** FGD SPARE CAPACITY INDICES

ABSORBER - %

. 0

** FGD SPARE COMPONENT INDICES

ABSORBER

. 0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

0/69 SYSTEM

** PROBLEMS/SOLUTIONS/COMMENTS

PROBLEMS WITH THE FGD SYSTEM ON BOILER NO. 4 INCLUDED BUILDUP AND PLUGGING-OF THE INLET DUCT WHERE HOT GASES ENTER THE SCRUBBERS, EROSION OF SCRUBBER WALLS, CORROSION OF SCRUBBERS INTERNALS, BUILDUP ON ID FAN ROTORS, AND PLUGGING OF DRAIN LINES, MARBLE BEDS, AND MIST ELIMINATORS. LOW SO2 REMOVAL WAS CAUSED BY OVERBURNING OF THE LIMESTONE AND DROPOUT OF THE LIME WITH THE ASH IN THE BOTTOM OF THE SCRUBBER.

THE SCRUBBERS WERE MODIFIED IN 1969 BY RAISING THE MIST ELIMINATOR AND ADDING SOOT BLOWERS IN THE INLET DUCT AND REHEATER TO REDUCE PLUGGING. NEW SPRAY NOZZLES WERE ALSO INSTALLED. REHEATER PLUGGING WAS ELIMINATED BY REPLACING COPPER REHEAT COILS WITH A CARBON STEEL UNIT HAVING WIDELY SPACED FINS.

0/70 SYSTEM

** PROBLEMS/SOLUTIONS/COMMENTS

MAJOR MODIFICATIONS IN 1970 WERE SANDBLASTING AND COATING OF THE INTERIOR OF THE SCRUBBERS, REPLACEMENT OF ALL INTERNAL STEEL PIPES WITH PLASTIC AND FIBERGLASS, AND REPLACEMENT OF STAINLESS STEEL MIST ELIMINATORS WITH FIBERGLASS. SINCE MIST ELIMINATOR PLUGGING WAS NOT COMPLETELY STOPPED, THE UNIT WAS WASHED MANUALLY EVERY NIGHT TO MAINTAIN THE REQUIRED MODULE SERVICE.

0/72 SYSTEM

** PROBLEMS/SOLUTIONS/COMMENTS

THE MODIFICATIONS IN THE SUMMER OF 1972 ON THE TWO FGD MODULES INCLUDED ENLARGEMENT OF THE CRYSTALLIZATION TANK, AND INSTALLATION OF NEW PLASTIC SPRAY NOZZLES, NEW SLURRY PUMPS AND STRAINERS, AND NEW MULTIPLE MIXERS IN THE TANK. PROBLEMS THAT REMAINED INCLUDED CORROSION, INEFFICIENT DAMPERS, EXPANSION JOINT FAILURE, MIST ELIMINATOR FOULING, RAPID EROSION OF THE SLURRY PUMP, AND VALVE FAILURE.

0/73 SYSTEM

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

OPERATION OF THE FGD SYSTEM SINCE THE FALL OF 1973 HAS BEEN THE MOST SUCCESSFUL TO DATE.

0/74 SYSTEM

** PROBLEMS/SOLUTIONS/COMMENTS

IN 1974 THIS UNIT WAS AVAILABLE FOR OPERATION 343 DAYS. 50% OF THE FUEL CONSUMED WAS COAL, 2% FUEL OIL, AND 48% NATURAL GAS.

0/75 SYSTEM

** PROBLEMS/SOLUTIONS/COMMENTS

DURING 1975 THIS UNIT WAS AVAILABLE FOR OPERATION 333 DAYS. 64% OF THE FUEL CONSUMED WAS COAL, 33% FUEL OIL, AND 33% NATURAL GAS.

THE UTILITY COMPLETED NEGOTIATIONS FOR A LOW-SULFUR COAL SUPPLY FROM SOUTHEAST WYOMING (MEDICINE BOW) IN 1974. THE HIGH-SULFUR KANSAS COAL WAS COMPLETELY PHASED OUT BY LATE SPRING OF 1975. THIS IMPROVED SCRUBBER OPERATIONS BECAUSE OF REDUCED SULFUR REMOVAL REQUIREMENTS AND THE ALKALINE SPECIES IN THE NEW COAL REDUCED THE AMOUNT OF NECESSARY LIMESTONE ADDITION.

6/75 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

STATION LOAD IS REDUCED TO 50% EVERY NIGHT. THEREFORE, ONE OF THE MODULES CAN BE TAKEN OFF-LINE NIGHTLY FOR CLEANING OR REPAIR. WYOMING COAL (0.5% SULFUR) IS NOW BEING BURNED IN THE BOILER FURNACE. SOME NATURAL GAS HAS BEEN BURNED SINCE JUNE 20, 1975.

7/75 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

EACH MODULE HAS BEEN SHUT DOWN ONCE PER WEEK FOR INSPECTION AND CLEAN-UP.

8/75	SYSTEM	744
9/75	SYSTEM	720
10/75	SYSTEM	744
11/75	SYSTEM	720
12/75	SYSTEM	744
1/76	SYSTEM	744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY IS REPLACING THE LINESTONE INJECTION FGD SYSTEM WITH A ROD-DECK VENTURI/SPRAY TOWER FGD SYSTEM. THE NEW SYSTEM WILL BE BROUGHT ON LINE IN EARLY JANUARY 1977.

2/76 SYSTEM 696 3/76 SYSTEM 744

KANSAS POWER & LIGHT: LAWRENCE 4 (CONT.)

				PERFORMA	VCE DATA						
PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% RE	MOVAL	PER	BOILER	FGD	CAP.
									HOURS		FACTOR
	000000		are								
4/76	SYSTEM							720			
5/76	SYSTEM							744			
6/76	SYSTEM							720			
7/76	SYSTEM							744			
8/76	SYSTEM							744			
	_										
9/76	SYSTEM							720			

** PROBLEMS/SOLUTIONS/COMMENTS

A SCHEDULED UNIT OUTAGE BEGAN IN MID-SEPTEMBER FOR A TURBINE OVERHAUL. THE UNIT IS SCHEDULED TO COME BACK ON LINE IN EARLY JANUARY.

10/76	SYSTEM	744
11/76	SYSTEM	720
12/76	SYSTEM	744
1/77	SYSTEM	744

** PROBLEMS/SOLUTIONS/COMMENTS

THE NEW LIMESTONE FGD SYSTEM BECAME COMMERCIALLY OPERABLE IN EARLY JANUARY 1977. THE UTILITY REPORTED THAT BOTH PARTICULATE AND SO2 REMOVALS IN THE ROD-DECK VENTURI/SPRAY TOWER SCRUBBING UNIT ARE QUITE SATISFACTORY.

2/77 SYSTEM 672 3/77 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

MINOR PROBLEMS HAVE BEEN RELATED TO MAINTAINING DESIRED SOLIDS LEVEL IN THE MAKE-UP TANK. MODIFICATIONN PLANS INCLUDE CESSATION OF SLURRY DILUTION, WHICH CURRENTLY PRECEDES THE INTRODUCTION OF THE FRESH LIMESTONE SLURRY INTO THE RECIRCULATION LOOP. THE UTILITY PLANS TO PUMP THE 35% SOLIDS SLURRY DIRECTLY FROM THE SLURRY TANK INTO THE RECIRCULATION LOOP.

CURRENTLY SEVERAL DIFFERENT MAKES OF SLURRY PUMPS ARE BEING USED. ALL ARE FUNCTIONING WELL SO FAR. THE PUMPS HAVE NOT BEEN IN SERVICE LONG ENOUGH FOR COMPARISONS TO BE DRAWN.

4/77 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE SCRUBBER WAS NOT REQUIRED FOR SERVICE DURING THE REPORT PERIOD BECAUSE NATURAL GAS WAS FIRED IN THE BOILER.

5/77 SYSTEM 744 6/77 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

MIST ELIMINATOR CRACKS HAVE BEEN A PROBLEM.

A COMPRESSOR BREAKDOWN IN THE RECYCLE TANK AIR AGITATION SYSTEM AND THE

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILEN FGD CAP.

SO2 PART. HOURS HOURS FACTOR

RECYCLE TANK STRAINER SCREEN WASH HAVE BEEN PROBLEM AREAS. THE WASH

RECYCLE TANK STRAINER SCREEN WASH HAVE BEEN PROBLEM AREAS. THE WASH SYSTEM HAS BEEN TWISTING OFF UNDER WATER PRESSURE.

SOOT BLOWER PROBLEMS WERE ENCOUNTERED.

THE DENVER SLURRY PUMPS ARE EXPERIENCING SOME ON-GOING PROBLEMS, WHILE THE ALLEN-SHERMAN-HOFF PUMPS ARE OPERATING SATISFACTORILY.

7/77 SYSTEM 744

8/77 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER BURNED NATURAL GAS THROUGHOUT AUGUST.

THE MIST ELIMINATOR CRACKS HAVE BEEN REPAIRED.

THE RECYCLE TANK STRAINER PROBLEMS PERSISTED AND THE AIR AGITATION SYSTEM COMPRESSOR WAS MALFUNCTIONING RESULTING IN SOLIDS SETTLING IN THE RECYCLE TANK

THE DENVER SLURRY PUMPS ARE FUNCTIONING ADEQUATELY AT PRESENT. THE PUMP GLAND PACKINGS ARE BEING REDESIGNED.

9/77 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE NO. 4 BOILER HAS BEEN FIRING 100% NATURAL GAS FOR ALL BUT 8 TO 10 DAYS SINCE THE BEGINNING OF APRIL 1977. AS OF SEPTEMBER 15 THE UNIT BEGAN BURNING COAL AGAIN.

10/77 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE SYSTEM LOAD WAS CUT BACK TO 50% IN OCTOBER BECAUSE A NEW COOLING TOWER IS BEING CONSTRUCTED.

11/77 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

ON NOVEMBER 15 A MAJOR FGD SYSTEM OVERHAUL TOOK PLACE WHILE THE TURBINE WAS DOWN FOR INSPECTION AND THE NEW COOLING TOWER WAS BEING CONNECTED.

12/77 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT CAME BACK ON LINE DECEMBER 20 AT FULL CAPACITY. THE TURBINES WERE BALANCED DURING DECEMBER.

1/78 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM OPERATED WITHOUT ANY PROBLEMS OTHER THAN SOME FREEZING OF THE PIPELINES.

THICKENER DISCHARGE LINE FREEZING CAUSED CLARIFIER PLUGGING.

2/78 SYSTEM 672

KANSAS POWER & LIGHT: LAWRENCE 4 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE THICKENER UNDERFLOW LINE IS STILL FROZEN AND TWO 3 INCH DIAMETER FIRE HOSES ARE BEING USED TO PUMP THE UNDERFLOW SOLIDS TO THE POND.

3/78	SYSTEM				744		
4/78	A B	100.0 100.0	100.0 100.0	100.0 100.0			
	SYSTEM	100.0	100.0	100.0	720	720	720
5/78	A B	100.0 100.0	100.0 100.0	100.0 100.0			
	SYSTEM	100.0	100.0	100.0	744	744	744
6/78	A B	100.0 100.0	100.0 100.0	100.0 100.0			
	SYSTEM	100.0	100.0	100.0	720	72 0	720
7/78	A	100.0	100.0	100.0			
	B System	100.0 100.0	100.0 100.0	100.0 100.0	744	744	744

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER AND FGD SYSTEM BOTH OPERATED THROUGHOUT JUNE AND JULY WITHOUT ANY FORCED OUTAGES.

8/78	A	100.0	100.0	100.0			
	В	100.0	100.0	100.0			
	SYSTEM	100.0	100.0	100.0	744	744	744
9/78	A	100.0	100.0	63.0			
	В	100.0	100.0	63.0			
	SYSTEM	100.0	100.0	63.0	720	456	456

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE SYSTEM RAN WITH NO FORCED OUTAGES DURING AUGUST AND SEPTEMBER.

THE UNIT WAS DOWN THE LAST WEEK AND A HALF IN SEPTEMBER FOR A SCHEDULED FALL TURBINE/BOILER OUTAGE. ROUTINE MAINTENANCE INCLUDED BOILER AND TURBINE CLEANING AND REPAIR.

10/78	SYSTEM	744	5 76
11/78	SYSTEM	720	720
12/78	SYSTEM	744	744

** PROBLEMS/SOLUTIONS/COMMENTS

AN EPA SPONSORED CONTINUOUS MONITORING TEST BEGAN AT THIS UNIT AT THE BEGINNING OF DECEMBER AND WILL CONTINUE THROUGH THE END OF JANUARY. THE TEST INVOLVES 24 HOUR MONITORING OF SO2, OPACITY AND NOX.

1/79 SYSTEM 744

672

672

564

KANSAS POWER & LIGHT: LAWRENCE 4 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

AN ID FAN WAS FORCED OUT OF SERVICE ON JANUARY 5 FORCING THE UNIT TO OPERATE AT 50% CAPACITY. THE FAN IS EXPECTED TO BE REPLACED BY JANUARY 12.

2/79 A 96.0 96.0 96.0 B 71.0 71.0 71.0 SYSTEM 84.0 84.0 84.0

** PROBLEMS/SOLUTIONS/COMMENTS

ONE MODULE WAS FORCED OUT OF SERVICE FOR TWO DAYS WHEN ITS TANK AGITATOR FAILED.

ONE MODULE WAS FORCED OUT OF SERVICE FOR AN EIGHT DAY PERIOD DUE TO A FAN MOTOR MALFUNCTION

3/79 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

UNIT 4 EXPERIENCED A MOTOR FAILURE ON AN ID FAN DURING THE FEBRUARY-MARCH PERIOD.

 4/79
 SYSTEM
 720

 5/79
 SYSTEM
 744

 6/79
 SYSTEM
 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE SYSTEM RAN WELL. THE ONLY FGD SYSTEM RELATED OUTAGES WERE DUE TO A MIXER FAILURE AND GENERAL MAINTENANCE.

7/79 SYSTEM 744 8/79 SYSTEM 744 9/79 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE THIRD QUARTER AN OUTAGE WAS CAUSED BY MIXER MOTOR AND OTHER MIXER RELATED PROBLEMS. DURING THE OUTAGE MAINTENANCE WAS DONE ON THE BOILER AND SCRUBBERS AND REPAIR WORK WAS DONE ON THE MIXERS.

10/79 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS OPERATED AT HALF LOAD DURING THE LAST WEEK OF SEPTEMBER AND WAS SHUT DOWN COMPLETELY IN EARLY OCTOBER FOR THE ANNUAL FALL OUTAGE.

11/79 SYSTEM 720 12/79 SYSTEM 744

KANSAS POWER & LIGHT: LAWRENCE 4 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS FACTOR ______ ** PROBLEMS/SOLUTIONS/COMMENTS THE UNIT WAS DOWN FOR APPROXIMATELY 10 DAYS OF SCHEDULED OUTAGE FOR FALL MAINTENANCE. SOME AGITATOR SHAFT FAILURES OCCURRED IN THE REACTION TANK CAUSING MAINTENANCE ATTENTION. 1/80 SYSTEM 100.0 100.0 100.0 744 744 744 2/80 SYSTEM 100.0 100.0 100.0 696 696 696 3/80 SYSTEM 100.0 100.0 100.0 744 744 744

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR PROBLEMS WERE REPORTED FOR THE LAWRENCE 4 SCRUBBER DURING THE FIRST QUARTER 1980.

4/80 SYSTEM 100.0 100.0 100.0 80.0 720 576 576

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER WAS OFF LINE FOR SIX DAYS IN APRIL FOR A SCHEDULED INSPECTION. DURING THE BOILER OUTAGE GENERAL MAINTENANCE WAS PERFORMED ON THE FGD SYSTEM.

5/80 SYSTEM 100.0 100.0 100.0 100.0 744 744. 744 6/80 SYSTEM 100.0 100.0 100.0 100.0 720 720 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE FGD SYSTEM OPERATED 100% OF THE TIME IN MAY AND JUNE

7/80 SYSTEM 96.8 96.8 96.8 96.8 744 744 720 54.8

** PROBLEMS/SOLUTIONS/COMMENTS

A STORAGE TANK ERODED COMPLETELY THROUGH CAUSING A TWO DAY OUTAGE IN JULY.

8/80 SYSTEM 100.0 100.0 100.0 100.0 744 744 744 50.2

** PROBLEMS/SOLUTIONS/COMMENTS

NO PROBLEMS WERE ENCOUNTERED WITH THE FGD SYSTEM OR THE BOILER DURING AUGUST.

9/80 SYSTEM 96.9 100.0 100.0 40.3 720 290 290 16.4

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER WAS OUT OF SERVICE FOR APPROXIMATELY 17 DAYS FOR A BOILER INSPECTION.

ECONOMIZER WELD REPAIRS CAUSED THE SYSTEM TO REMAIN OUT OF SERVICE FOR 22 HOURS.

10/80 SYSTEM 100.0 100.0 100.0 744 744 744

744

KANSAS POWER & LIGHT: LAWRENCE 4 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE MONTH OF OCTOBER.

11/80 SYSTEM 100.0 100.0 100.0 89.7 720 646 646

** PROBLEMS/SOLUTIONS/COMMENTS

DURING NOVEMBER THE BOILER WAS OUT OF SERVICE APPROXIMATELY 74 HOURS DUE TO TUBE LEAKS. THE FGD SYSTEM WAS AVAILABLE 100% DURING THIS TIME.

12/80 SYSTEM 100.0 100.0 100.0 98.1 744 730 730

** PROBLEMS/SOLUTIONS/COMMENTS

DURING DECEMBER 14 HOURS OF OUTAGE TIME WAS DUE TO TRANSFORMER PROBLEMS. THE FGD SYSTEM WAS AVAILABLE THE ENTIRE MONTH.

1/81 SYSTEM

2/81 SYSTEM 672

3/81 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

LAWRENCE 4 WAS ON COLD STANDBY MUCH OF THE JANUARY-MARCH PERIOD AND THEREFORE DID NOT SEE MUCH OPERATION. UTILITY REPORTED THERE WERE NO FGD SYSTEM RELATED OUTAGES DURING THE QUARTER.

 4/81
 SYSTEM
 720

 5/81
 SYSTEM
 744

 6/81
 SYSTEM
 720

 7/81
 SYSTEM
 744

 8/81
 SYSTEM
 744

 9/81
 SYSTEM
 720

** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE MONTH OF SEPTEMBER, LAWRENCE 4 WAS ON COLD STANDBY FROM THE THIRD TO THE TWENTY FIRST. NO FGD SYSTEM-RELATED PROBLEMS WERE REPORTED FOR THIS UNIT DURING THE SECOND AND THIRD QUARTERS OF 1981.

 10/81
 SYSTEM
 744

 11/81
 SYSTEM
 720

 12/81
 SYSTEM
 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT BOILER OPERATIONS WERE NOT CURTAILED OR REDUCED AS A RESULT OF THE FGD SYSTEM DURING THE ENTIRE FOURTH QUARTER 1981.

1/82 SYSTEM 744

2/82 SYSTEM 672

KANSAS POWER & LIGHT: LAWRENCE 4 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

3/82 SYSTEM

744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE FIRST QUARTER 1982. SOMETIME DURING THE FIRST AND/OR SECOND QUARTER 1982, THE UNIT WILL BE SHUTDOWN FOR A SCHEDULED 2 WEEK SPRING OUTAGE.

4/82	SYSTEM	720
5/82	SYSTEM	744
6/82	SYSTEM	720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE SECOND QUARTER 1982.

7/82	SYSTEM	744
8/82	SYSTEM	744
9/82	SYSTEM	720
10/82	SYSTEM	744
11/82	SYSTEM	720
12/82	SYSTEM	744
1/83	SYSTEM	744
2/83	SYSTEM	672
3/83	SYSTEM	744

** PROBLEMS/SOLUTIONS/COMMENTS

OVER THE PAST YEAR THE LAWRENCE 4 AND 5 FGD SYSTEMS HAVE OPERATED WITH NO MAJOR FROBLEMS. THERE HAVE BEEN SOME CHRONIC MINOR PROBLEMS WITH SFRAY HEADER PLUGGING. THERE MAY BE SOME MODIFICATIONS PERFORMED AT SOME POINT IN THE FUTURE TO MINIMIZE THE PROBLEM.

THE DOWNSTREAM DUCTWORK IN BOTH THE LAWRENCE 4 AND 5 FGD SYSTEMS HAS BEEN EXPERIENCING CORPOSION THAT WILL REQUIRE SOME DEGREE OF REPLACEMENT. THE CORROSION IS NOT RELATED TO CHLORIDES. A TIME TABLE FOR THE REPAIR WORK WAS NOT REPORTED BY THE UTILITY.

4/83	SYSTEM	720
5/83	SYSTEM	744
6/83	SYSTEM	720
7/83	SYSTEM	744
8/83	SYSTEM	744
9/83	SYSTEM	720

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HCURS HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED FORCED OUTAGES WERE ENCOUNTERED DURING THE PERIOD OF APRIL THROUGH SEPTEMBER.

THE NEXT UNIT OUTAGE IS SCHEDULED TO BEGIN ON OCTOBER 23 AND LAST FROM TWO TO THREE WEEKS. DURING THE OUTAGE, THE UTILITY PLANS TO DO SOME TEMPORARY PATCH WORK ON THE ABSORBER OUTLET DUCTING. THE UTILITY STATED THAT THIS DUCTWORK WILL EVENTUALLY NEED SOME MAJOR REPLACEMENT WORK (PLANNED FOR SOMETIME IN 1984).

 10/83
 SYSTEM
 744

 11/83
 SYSTEM
 720

 12/83
 SYSTEM
 744

** PROBLEMS/SOLUTIONS/COMMENTS

LAWRENCE 4 WAS ON LINE LESS THAN 600 HOURS DURING THE FOURTH QUARTER OF 1983 DUE TO LOW POWER DEMAND.

 1/84
 SYSTEM
 744

 2/84
 SYSTEM
 696

 3/84
 SYSTEM
 744

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE REPORTED DURING THE FIRST QUARTER OF 1984.

 4/84
 SYSTEM
 720

 5/84
 SYSTEM
 744

 6/84
 SYSTEM
 720

** PROBLEMS/SOLUTIONS/COMMENTS

A MAJOR OUTAGE OCCURRED DURING MAY AND JUNE TO REPLACE CORRODING OUTLET DUCTWORK IN THE REHEAT SECTION. CARBON STEEL DUCTS WERE REPLACED WITH FIBERGLASS.

7/84 SYSTEM 744 8/84 SYSTEM 744 9/84 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT OVERALL FGD SYSTEM AVAILABILITY FOR THE FIRST THREE QUARTERS OF 1984 WAS ABOVE 90%.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

KANSAS POWER & LIGHT COMPANY NAME LAWRENCE DIANT NAME UNIT NUMBER LAWRENCE CITY KANSAS STATE REGULATORY CLASSIFICATION 43. (.100 LB/ffmbtu) 215. (.500 LB/ffmbtu) ***** (***** LB/fmbtu) PARTICULATE EMISSION LIMITATION - NG/J 43. 215. **** SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J 576 420 400 NET PLANT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW NET UNIT GENERATING CAPACITY W/FGD - MW NET UNIT GENERATING CAPACITY WO/FGD - MW 495 EQUIVALENT SCRUBBED CAPACITY - MW 420 ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER COMBUSTION ENGINEERING BOILER TYPE PULVERIZED COAL CYCLING 599.78 BOILER SERVICE LOAD DESIGN BOILER FLUE GAS FLOW - CU.M/S BOILER FLUE GAS TEMPERATURE - C (1271000 ACFM) 148.9 (300 F) 107. (350 FT) (350 FT) STACK HEIGHT - M CARBON STEEL STACK SHELL STACK TOP DIAMETER - M 4.9 (16.0 FT) ** FUEL DATA COAL FUEL TYPE SUBBITUMINOUS FUEL GRADE AVERAGE HEAT CONTENT - J/G 23260. (10000 BTU/LB) RANGE HEAT CONTENT - BTU/LB ***** AVERAGE ASH CONTENT - X 9.80 RANGE ASH CONTENT - % 9.8-16.0 AVERAGE MOISTURE CONTENT - % 11.A0 RANGE MOISTURE CONTENT - % **** AVERAGE SULFUR CONTENT - % .55 RANGE SULFUR CONTENT - % 0.55-0.90 AVERAGE CHLORIDE CONTENT - % .03 RANGE CHLORIDE CONTENT - % *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER Λ TYPE NONE ** ESP NUMBER Λ TYPE NONE ** PARTICLE SCRUBBER NUMBER 2 NUMBER OF SPARES INITIAL START-UP DATE 4/78 GENERIC TYPE VENTURI TOWER SPECIFIC TYPE VARIABLE-THROAT/VERTICALLY-ADJUSTABLE ROD DECKS TRADE NAME/COMMON NAME ROD SCRUBBER SUPPLIER COMBUSTION ENGINEERING DIMENSIONS - FT 5.0 X 37.0 SHELL GENERIC MATERIAL STAINLESS STEEL SHELL SPECIFIC MATERIAL AUSTENITIC LINER GENERIC MATERIAL NONE LINER SPECIFIC MATERIAL N/A GAS CONTACTING DEVICE TYPE GAS CONTACTING DEVICE TIPE
NUMBER OF CONTACTING ZONES 1
LIQUID RECIRCULATION RATE - LITER/S 655.2
2.2 TYPE 316L STAINLESS STEEL RODS (10400 GPM) (16.4 GAL/1000ACF) PH CONTROL ADDITIVE LIMESTONE SLURRY 2.2 (9.0 IN-H20) 15.2 (50.0 FT/S) PRESSUPE DROP - KPA SUPERFICIAL GAS VELOCITY - M/S

```
KANSAS POWER & LIGHT: LAWRENCE 5 (CONT.)
                                               299.7
148.9
    INLET GAS FLOW RATE - CU.M/S
                                                              ( 635000 ACFM)
    INLET GAS TEMPERATURE - C
                                                              ( 300 F)
    PARTICLE REMOVAL EFFICIENCY - %
                                                  99.0
*** FGD SYSTEM
 ** GENERAL DATA
    SALEABLE PRODUCT/THROWAWAY PRODUCT
                                               THROWAWAY PRODUCT
    SO2 REMOVAL MODE
                                               WET SCRUBBING
                                               LIMESTONE
    PROCESS TYPE
                                               NONE
    PROCESS ADDITIVES
    SYSTEM SUPPLIER
                                               COMBUSTION ENGINEERING
    A-E FIRM
                                               BLACK & VEATCH
    DEVELOPMENT LEVEL
                                               FULL SCALE
    NEW/RETROFIT
                                               RETROFIT
    UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 98.90
    UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                  52.00
    CURRENT STATUS
    COMMERCIAL START-UP
                                                4/78
    INITIAL START-UP
                                                4/78
    CONTRACT AWARDED
                                                9/69
 ** DESIGN AND OPERATING PARAMETERS
 ** QUENCHER/PRESATURATOR
                                                0
    NUMBER
 ** ABSORBER
                                                2
    NUMBER
    NUMBER OF SPARES
                                                n
                                               SPRAY TOWER
    GENERIC TYPE
                                               OPEN COUNTERCURRENT SPRAY
    SPECIFIC TYPE
    TRADE NAME/COMMON TYPE
                                               N/A
                                               COMBUSTION ENGINEERING
    SUPPLIER.
    SHELL GENERIC MATERIAL
                                               STAINLESS STEEL
                                               AUSTENITIC
    SHELL SPECIFIC MATERIAL
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                               TYPE 316L
                                               NONE
    LINER GENERIC MATERIAL
    LINER SPECIFIC MATERIAL
                                               N/A
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                               N/A
    GAS CONTACTING DEVICE TYPE
                                               N/A
    NUMBER OF CONTACTING ZONES
                                                1
    LIQUID RECIRCULATION RATE - LITER/S
                                                655.
                                                             (10400 GPM)
    L/G RATIO - L/CU.M
                                                  2.6
                                                             ( 19.1 GAL/1000 ACF)
                                                             ( .8 IN-H20)
( 6.0 FT/S)
    GAS-SIDE PRESSURE DROP - KPA
                                                    . 2
    SUPERFICAL GAS VELOCITY - M/SEC
                                                   1.8
    INLET GAS FLOW - CU. M/S
                                                 256.71
                                                             ( 544000 ACFM)
    INLET GAS TEMPERATURE - C
                                                  52.2
                                                             ( 126 F)
    502 REMOVAL EFFICIENCY - %
                                                  70.0
 ** MIST ELIMINATOR
    PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                              PRIMARY COLLECTOR
    NUMBER PER SYSTEM
                                                2
    NUMBER OF SPARES PER SYSTEM
                                                0
    NUMBER PER MODULE
                                                1
    GENERIC TYPE
                                               IMPINGEMENT
    SPECIFIC TYPE
                                               BAFFLE
                                               CLOSED VANE
    TRADE NAME/COMMON TYPE
                                               HORIZONTAL
    CONFIGURATION
    NUMBER OF STAGES
    NUMBER OF PASSES PER STAGE
                                                   2
                                                                 .3 FT)
    FREEBOARD DISTANCE - M
                                                    .09
    DISTANCE BETWEEN STAGES - CM
                                                 30.48
                                                              (12.0 IN)
    DISTANCE BETWEEN VANES - CM
                                                   8.9
                                                              ( 3.50 IN)
                                                 90
    VANE ANGLES - DEGREES
```

. 2

POND RECYCLE

FIBER-REINFORCED POLYESTER

1.8

ORGANIC

ONCE/DAY

(1.0 IN-H20)

(6.0 FT/S)

PRESSURE DROP - KPA

WASH WATER SOURCE

WASH FREQUENCY

SUPERFICAL GAS VELOCITY - M/S

CONSTRUCTION MATERIAL GENERIC TYPE

CONSTRUCTION MATERIAL SPECIFIC TYPE

```
12.6 ( 200 GAL/MIN)
     WASH PATE - L/S
** PFHFATFR
                                                           2
    NUMBER
     NUMBER PER MODULE
                                                          IN-LINE
     GENERIC TYPE
     SPECIFIC TYPE
                                                         HOT WATER
                                                         FIN TUBE
     TRADE NAME/COMMON TYPE
                                                           13.9 ( 25 F)
551.18 (1168000 ACFM)
51.7 ( 125 F)
65.6 ( 150 F)
     TEMPERATURE INCREASE - C
     INLET FLUE GAS FLOW RATE - CU. M/S
INLET FLUE GAS TEMPERATURE - C
     OUTLET FLUE GAS TEMPERATURE - C
     NUMBER OF BUNDLES PER BANK
                                                            2
     NUMBER OF TUBES PER BUNDLE
                                                            66
     CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL CONSTRUCTION MATERIAL SPECIFIC TYPE AISI 1110
** FANS
    NUMBER
     DESIGN
                                                          CENTRIFUGAL
                                                           AMERICAN STANDARD
     SUPPLITER
     FUNCTION
                                                          BOOSTER
                                                          INDUCED DRAFT
     APPLICATION
     SERVICE
                                                          DRY
                                                          283.14 ( 600000 ACFM)
65.6 ( 150 F)
     FLUE GAS FLOW RATE - CU.M/S
     FLUE GAS TEMPERATURE - C
     CONSTRUCTION MATERIAL GENERIC TYPE
                                                      CARBON STEEL
** DAMPERS
     GENERIC TYPE
                                                          LOUVER
     SPECIFIC TYPE
     CONSTRUCTION MATERIAL GENERIC TYPE

CONSTRUCTION MATERIAL SPECIFIC TYPE

LINER GENERIC MATERIAL TYPE

LINER SPECIFIC MATERIAL TYPE

NONE
                                                          HIGH STRENGTH LOW ALLOY [HSLA]
     LINER SPECIFIC MATERIAL TYPE
                                                          N/A
** DAMPERS
     GENERIC TYPE
                                                          LOUVER
     SPECIFIC TYPE
     CONSTRUCTION MATERIAL SPECIFIC TYPE

CONSTRUCTION MATERIAL SPECIFIC TYPE

LINER GENERIC MATERIAL TYPE

CARBON STEEL

HIGH STRENGTH
                                                         HIGH STRENGTH LOW ALLOY [HSLA]
     LINER SPECIFIC MATERIAL TYPE
                                                          N/A
** DAMPERS
     GENERIC TYPE
                                                          LOUVER
     SPECIFIC TYPE
                                                        CARBON STEEL
     CONSTRUCTION MATERIAL GENERIC TYPE
     CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
LINER GENERIC MATERIAL TYPE
                                                          HIGH STRENGTH LOW ALLOY [HSLA]
     LINER GENERIC MATERIAL TYPE
                                                          NONE
     LINER SPECIFIC MATERIAL TYPE
                                                          N/A
** DUCTWORK
     LOCATION
                                                         SCRUBBER THIFT
      SHELL GENERIC MATERIAL TYPE
                                                          CARBON STEEL
      SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
                                                        HIGH STRENGTH LOW ALLOY [HSLA]
                                                          NONE
      LINER SPECIFIC MATERIAL TYPE
                                                          N/A
** DUCTWORK
     LOCATION
                                                         SCRUBBER OUTLET
      SHELL GENERIC MATERIAL TYPE
      SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
                                                          CARBON STEEL
                                                        HIGH STRENGTH LOW ALLOY [HSLA]
      LINER GENERIC MATERIAL TYPE
                                                          NONE
      LINER SPECIFIC MATERIAL TYPE
                                                          N/A
** DUCTWORK
     LOCATION
                                                         BYPASS
      SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
TIMER GENERIC MATERIAL TYPE
                                                         CARBON STEEL
HIGH STRENGTH LOW ALLOY [HSLA]
      LINER GENERIC MATERIAL TYPE
                                                          NONE
```

LINER SPECIFIC MATERIAL TYPE N/A

** REAGENT PREPARATION EQUIPMENT

WET BALL MILL FUNCTION COMPARTMENTED DEVICE DEVICE TYPE ND NUMBER 2

FULL LOAD DRY FEED CAPACITY - M.TONS/HR 21.8 (24 TPH) 60.0

PRODUCT QUALITY - % SOLIDS

** TANKS

SERVICE NUMBER VENTURI & ABSORBER RECYCLE 1 ADDITIVE STORAGE 1 ADDITIVE DILUTION **** MILL SUMP **** MILL PRODUCT *** RECLAIMED WATER ****

** PUMPS

SERVICE NUMBER -----REACTION/RECYCLE TANK BLEED **** VENTURI RECIRCULATION 2 MIST ELIMINATOR WASH **** MILL SLURRY 2 ADDITIVE DILUTION ABSORBER RECIRCULATION 2 ADDITIVE TRANSFER ******** ADDITIVE STORAGE **** ADDITIVE FEED *** RECLAIMED WATER

** SOLIDS CONCENTRATING/DEWATERING

DEVICE NONE

*** SLUDGE

** TREATMENT

FORCED OXIDATION METHOD REACTION TANK DEVICE PROPRIETARY PROCESS N/A INLET QUALITY - % 10.0

** DISPOSAL

INTERIM NATURE TYPE DNO LOCATION ON-SITE SITE TRANSPORTATION METHOD PIPELINE SITE TREATMENT NONE

** DISPOSAL

NATURE FINAL TYPE POND ON-SITE LOCATION

SITE TRANSPORTATION METHOD OVERFLOW FROM INTERIM SLUDGE POND

NONE SITE TREATMENT

** PROCESS CONTROL AND INSTRUMENTATION

CHEMICAL PARAMETERS PH, SO2 CONCENTRATION PHYSICAL VARIABLES PERCENT SOLIDS, SLURRY FLOW, PRESSURE CHANGE ACR CONTROL LEVELS PH 6.5 MCMITOR LOCATION PH PROBES IN REACTION TANKS PROCESS CONTROL MANNER AUTOMATIC FRCCESS CHEMISTRY MODE FEEDBACK

KANSAS POWER & LIGHT: LAWRENCE 5 (CONT.)

** WATER BALANCE WATER LOOP TYPE

CLOSED

** CHEMICALS AND CONSUMPTION

FUNCTION
NAME
PRINCIPAL CONSTITUENT
SOURCE/SUPPLIER
CONSUMPTION
POINT OF ADDITION

ABSORBENT LIMESTONE 93% CACO3, 7% MGCO3 LAWRENCE, KANSAS 4 TPH BALL MILL

** FGD SPARE CAPACITY INDICES

ABSORBER - %

۰.0

** FGD SPARE COMPONENT INDICES

ABSORBER

.0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

0/74 SYSTEM

** PROBLEMS/SOLUTIONS/COMMENTS

THE LAWRENCE 5 BOILER WAS ORIGINALLY EQUIPPED WITH A LIMESTONE INJECTION FGD SYSTEM MODELED AFTER THE FGD SYSTEM RETROFITED ONTO THE LAWPENCE 4 BOILER. CONSTRUCTION OF THE LAWRENCE 5 BOILER AND SCRUBBING SYSTEM BEGAN IN MARCH 1968 AND PROCEEDED SIMULTANEOUSLY WITH THE RETROFIT WORK ON LAWRENCE 4. INITIAL OPERATION OF THE LAWRENCE 5 BOILER AND SCRUBBING SYSTEM OCCURRED IN MARCH 1977. COMMERCIAL OPERATIONS WERE ACHIEVED IN NOVEMBER 1971 WITH THE COMPLETION OF THE SHAKEDOWN PHASE OF OPERATIONS.

THE LIMESTONE INJECTION FGD SYSTEM INCLUDED FACILITIES FOR PULVERIZING LIMESTONE AND THEN INJECTING IT INTO THE BOILER FURNACE CHAMBER FOR CALCINATION. THE FLUE GAS TRANSPORTS THE CALCINED LIMESTONE AND FLYASH TO THE SCRUEBER MODULES, EACH CONSISTING OF A SINGLE MARBLE BED EQUIPPED WITH OVERFLOH POTS FOR DRAINAGE OF RECIRCULATING SLURRY, FOR PARTICLE AND SULFUR DIOXIDE REMOVAL. THE CLEANED GASES THEN PASSED THROUGH A SET OF MIST ELIMINATORS, REHEATERS, AND INDUCED DRAFT FANS BEFORE BEING DISCHARGED THROUGH THE STACKS TO THE ATMOSPHERE.

ALTHOUGH THE CONFIGURATION OF THIS ORIGINAL SYSTEM WAS FAIRLY SIMPLE, MANY OPERATING PROBLEMS AND DESIGN INADEQUACIES WERE ENCOUNTERED. IN THE INJECTION PROCESS IT WAS DIFFICULT TO ACHIEVE SATISFACTORY CONTROL OF THE LIMESTONE CALCINATION AS WELL AS THE AMOUNT OF LIME/LIMESTONE CARRIED BY THE FLUE GAS INTO THE TAIL-END SCRUBBERS. THIS PROBLEM WAS FURTHER COMPLICATED WHEN THE BOILER WAS FIRED WITH A VARIABLE COMBINATION OF COAL, NATURAL GAS AND OIL.

THE FGD SYSTEM WAS MODIFIED A NUMBER OF TIMES THROUGHOUT ITS LIFE AND WAS LATER ABANDONED FOR A NEW SECOND-GENERATION SCRUBBER DESIGN DEVELOPED BY THE SYSTEM SUPPLIER. THE LIMESTONE INJECTION SYSTEM OPERATED UNTIL MARCH 20, 1978 WHEN IT WAS SHUTDOWN TO TIE THE NEW ROD DECK-VENTURI/SPRAY TOWER SCRUBBING SYSTEM INTO THE FLUE GAS PATH.

8/74 SYSTEM

744

** PROBLEMS/SOLUTIONS/COMMENTS

ONE MODULE WAS ISOLATED TO PERFORM FLOW DISTRIBUTION TESTS THROUGH THE MARBLE BED IN AUGUST.

THE MIST ELIMINATOR WASH SYSTEM IS NOT EFFECTIVE. THE MIST ELIMINATORS HAVE HAD TO BE CLEANED MANUALLY.

THE BOILER IS CURRENTLY BEING FIRED WITH GAS AND OIL.

9/74 SYSTEM

720

10/74 SYSTEM

744

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT OPERATED ON GAS AND OIL UNTIL OCTOBER 12 WHEN COAL WAS BURNED AGAIN.

POOR GAS DISTRIBUTION THROUGH THE MARBLE BEDS AND AMONG THE EIGHT MODULES IS STILL A PROBLEM AREA. THE SYSTEM SUPPLIER HAS COMPLETED THE GAS DISTRI-BUTION TEST AND IS CURRENTLY MODIFYING THE GAS FLOW PATTERN THROUGH THE

11/74 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS AVAILABLE NEARLY 100% OF NOVEMBER. GAS DISTRIBUTION PROBLEMS ARE CONTINUING.

12/74 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

SINCE OCTOBER 12 THE UNIT HAS OPERATED ON A BLEND OF KANSAS AND WYOMING COAL. THE FGD SYSTEM HAS BEEN AVAILABLE APPROXIMATELY 97% OF THE OCTOBER-DECEMBER PERIOD. SO2 REMOVAL EFFICIENCY HAS BEEN APPROXIMATELY 75%.

MODIFICATIONS TO IMPROVE GAS DISTRIBUTION WITHIN AND AMONG THE MODULES HAVE NOT COMPLETELY SOLVED THE PROBLEM.

PUMP RUBBER LINING FAILURES OCCURRED DURING DECEMBER. SCRAPS OF RUBBER WERE DISCOVERED AT THE DISCHARGE PIPE OF THE SLURRY RECYCLE PUMPS.

1/75 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT BURNED A MIXTURE OF 70% WYOMING AND 30% KANSAS COAL DURING JAN-UARY.

2/75 SYSTEM 672

3/75 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT BURNED WYOMING COAL HAVING 0.5% SULFUR DURING MARCH.

4/75 SYSTEM 720

5/75 SYSTEM 744

6/75 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM SHUTDOWN FOR MOST OF JUNE FOR A MAJOR REBUILD OF THE SPRAY SYSTEMS IN ALL EIGHT MODULES. THE BOILER WAS FIRED WITH OIL AND THE FGD SYSTEM WAS BYPASSED.

7/75 SYSTEM .0 744 0 744

8/75 SYSTEM ۰.0 744 744 0

KANSAS POWER & LIGHT: LAWRENCE 5 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

OIL AND GAS WERE FIRED IN JULY AND AUGUST, RESULTING IN NO FGD OPERATION.

9/75 SYSTEM 720 10/75 SYSTEM 744

** PROBLEMS/SQLUTIONS/COMMENTS

DURING THE SEPTEMBER-OCTOBER PERIOD THE BOILER WAS SHUT DOWN FOR A SHORT TIME TO PERFORM A BOILER INSPECTION AND TO MAKE SOME TURBINE REPAIRS. DURING PART OF THE PERIOD GAS AND OIL WERE BURNED IN THE BOILER FURNACE.

SLURRY RECYCLE TANK SCREENS WERE REPLACED DURING THE SEPTEMBER-OCTOBER PERIOD.

11/75 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

PROJECTIONS BY THE UTILITY FOR THIS UNIT CALL FOR 330 DAYS OF OPERATION ON 1976 WITH FUEL CONSUMPTION BEING 60% COAL, 25% FUEL OIL, AND 15% NATURAL GAS.

LIKE UNIT 4 THIS UNIT MAY BE CONVERTED TO A ROD-DECK VENTURI AND SPRAY TOWER SCRUBBING SYSTEM.

 12/75
 SYSTEM
 744

 1/76
 SYSTEM
 744

 2/76
 SYSTEM
 696

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY HAS DECIDED TO INSTALL A NEW ROD DECK-VENTURI/SPRAY TOWER FGD SYSTEM AT LAWRENCE 5.

3/76	SYSTEM	744
4/76	SYSTEM	720
5/76	SYSTEM	744
6/76	SYSTEM	720
7/76	SYSTEM	744
8/76	SYSTEM	744
9/76	SYSTEM	720
10/76	SYSTEM	744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE INSTALLATION OF THE NEW ROD AND SPRAY TOWER SCRUBBING SYSTEM IS NOW IN PROGRESS. THE SYSTEM WILL CONSIST OF TWO SCRUBBING TRAINS EACH HANDLING 50% OF THE FLUE GAS CAPACITY. FOUNDATION AND STRUCTURAL STEEL ERECTION HAS BEEN COMPLETED, AND SOME OF THE BREECHING HAS BEEN INSTALLED. THE UNIT WILL OPERATE IN A FULLY AUTOMATIC MODE.

744

KANSAS POWER & LIGHT: LAWRENCE 5 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

THE BOILER HAS BEEN OPERATING NO. 2 FUEL OIL IN ADDITION TO LOW SULFUR WYOMING COAL WHILE THE NEW SCRUBBING FACILITIES ARE BEING INSTALLED. THE ORIGINAL LIMESTONE INJECTION AND TAIL-END SCRUBBING SYSTEM IS STILL AVAIL-ABLE FOR SERVICE AND IS OPERATED WHEN THE UNIT FIRES COAL. THE SYSTEM TREATS FLUE GAS RESULTING FROM THE BURNING OF LOW SULFUR (0.5%) WYOMING COAL.

THE UTILITY REPORTED THAT C-E HAS ENCOUNTERED SOME PROBLEMS WORKING OUT AND FINE TUNING SOME OF THE INSTRUMENTATION LOGIC CIRCUITS.

11/76 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

12/76 SYSTEM

KP&L REPORTED THAT CONSTRUCTION OF THE NEW SCRUBBING SYSTEM IS STILL IN PROGRESS. THE ERECTION OF THE STRUCTURAL STEEL AND BREECHING IS CONTINUING. THE MODULES ARE NOW BEING ERECTED AT THE PLANT SITE, PARALLEL TO THE EXISTING MARBLE-BED SYSTEM.

1/77	SYSTEM	744
2/77	SYSTEM	672
3/77	SYSTEM	744
4/77	SYSTEM	720
5/77	SYSTEM	744
6/77	SYSTEM	720

** PROBLEMS/SOLUTIONS/COMMENTS

OPERATION OF THE EXISTING MARBLE BED SCRUBBERS HAS BEEN QUITE SATISFACTORY AND NEARLY PROBLEM FREE. THE CONNECTING DUCTWORK IS CURRENTLY BEING INSTALLED AS CONSTRUCTION CONTINUES ON THE NEW FGD SYSTEM. THE THO PARALLEL SCRUBBING MODULES EACH DESIGNED TO HANDLE 200 MW OF GENERATING CAPACITY ARE INSTALLED, AS ARE THE REHEATER TUBE BUNDLES. THE EXISTING MARBLE BED SCRUBBERS WILL BE REMOVED WHEN THE NEW SCRUBBING SYSTEM IS READY FOR SCRUBBING OPERATION.

7/77 SYSTEM 744 8/77 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

SOME OF THE NEW DUCTWORK IS IN PLACE. THE NEW SCRUBBER MODULES ARE IN IN PLACE AS ARE THE REHEATER TUBES. THE NO. 1 AND 8 MARBLE BED MODULES WILL SOON BE REMOVED BECAUSE THE SPACE IS NEEDED FOR FURTHER CONSTRUCTION.

OPERATIONS OF THE EXISTING FGD SYSTEM THROUGHOUT AUGUST HAVE BEEN GOOD.

9/77 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE CONSTRUCTION ON THE NEW SCRUBBER PLANT IS CONTINUING ACCORDING TO SCHEDULE AND IS EXPECTED TO BE COMPLETE BY APRIL 1978.

10/77 SYSTEM 744

11/77 SYSTEM 720

KANSAS POWER & LIGHT: LAWRENCE 5 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

JUE PART. NUURO NUURO PACITARIA PACI

** PROBLEMS/SOLUTIONS/COMMENTS

THE SYSTEM OPERATED ACCEPTABLY THROUGHOUT OCTOBER AND NOVEMBER.

12/77 SYSTEM 744

1/78 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE CONSTRUCTION OF THE ROD-DECK SCRUBBERS IS NOW COMPLETE. THE INLET DUCTWORK IS BEING INSTALLED, AND THE OUTLET DECTWORK WILL BE INSTALLED ALONG WITH ADDITIONAL CONTROLS DURING THE SCHEDULED OUTAGE IN APRIL 1978,

THE EXISTING FGD SYSTEM OPERATED WITHOUT SERIOUS PROBLEMS THROUGHOUT DECEMBER AND JANUARY. ONLY SIX MODULES ARE LEFT ON THE EXISTING SYSTEM. TWO WERE REMOVED TO MAKE ROOM FOR THE NEW SYSTEM.

2/78 SYSTEM 672

3/78 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE ORIGINAL FGD SYSTEM WAS PULLED OFF LINE ON MARCH 20 SO THAT THE NEW SCRUBBER-ABSORBER SYSTEM COULD BE TIED INTO THE GAS PATH. THIS NEW SYSTEM CONSISTS OF TWO MODULES EACH WITH A ROD SCCTION FOR PARTICULATE REMOVAL AND A SPRAY TOWER FOR SO2 REMOVAL. THE CAPACITY IS 210 MW EACH MODULE. INITAL OPERATION SHOULD BEGIN BY THE FIRST OF MAY.

4/78 SYSTEM 720

5/78 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE NEW UNIT WENT IN SERVICE ON APRIL 14 AND HAS OPERATED WITH NO OUTAGES SINCE START-UP.

6/78 SYSTEM 100.0 100.0 100.0 720

7/78 SYSTEM 100.0 100.0 100.0 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER OPERATED ALL BUT TWO DAYS OF THE JUNE-JULY PERIOD, WHEN A BOILER DRAIN LINE LEAK CAUSED AN OUTAGE.

THE FGD SYSTEM OPERATED THE ENTIRE TIME THE BOILER WAS ON-LINE, WITH NO REPORTED PROBLEMS.

8/78 SYSTEM 744

9/78 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE SYSTEM OPERATED WITH NO FORCED OUTAGES DURING THE AUGUST-SEPTEMBER PERIOD. THE UNIT WAS TAKEN OUT OF SERVICE AT THE END OF SEPTEMBER FOR A SCHEDULED TURBINE/BOILER INSPECTION. ROUTINE MAINTENANCE IS BEING PERFORMED ON THE BOILER AND TURBINE.

10/78 SYSTEM 744

720

KANSAS POWER & LIGHT: LAWRENCE 5 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

11/78 SYSTEM

THE FGD SYSTEM OPERATED THROUGHOUT OCTOBER AND NOVEMBER WITH ONLY ONE OUTAGE IN OCTOBER FOR AN ANNUAL ONE-WEEK BOILER/TURBINE INSPECTION.

12/78 SYSTEM 95.5 744 642 1/79 SYSTEM 744 2/79 SYSTEM 672

** PROBLEMS/SOLUTIONS/COMMENTS

A 30 HOUR OUTAGE WAS REQUIRED IN FEBRUARY TO REPAIR A RUPTURED PIPE IN THE FGD SYSTEM.

3/79 SYSTEM 744 4/79 SYSTEM 720 5/79 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS BROUGHT DOWN TO 50% CAPACITY FOR A SCHEDULED THREE WEEK OUTAGE IN MAY TO REBUILD AN AIR PREHEATER FAN MOTOR.

6/79 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE SYSTEM OPERATED WELL THROUGH JUNE. THE ONLY FGD SYSTEM RELATED OUTAGES WERE DUE TO RECYCLE TANK AGITATOR FAILURE AND GENERAL MAINTENANCE.

7/79 SYSTEM 744 8/79 SYSTEM 744 9/79 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT OPERATED NORMALLY THROUGHOUT THE THIRD QUARTER OF 1979. THE UNIT WILL BE SHUT DOWN FOR AN ANNUAL FALL OUTAGE ON OCTOBER 15. DURING THE OUTAGE SOME BOILER WORK WILL BE DONE. THE SCRUBBER WILL BE CLEANED AND MAINTENANCE WORK WILL BE PERFORMED ON THE RECYCLE TANK AGITATORS. THE OUTAGE IS TO LAST TWO WEEKS.

 10/79
 SYSTEM
 744

 11/79
 SYSTEM
 720

 12/79
 SYSTEM
 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS DOWN FOR APPROXIMATELY 10 DAYS OF SCHEDULED OUTAGE FOR FALL MAINTENANCE DURING THE SECOND QUARTER OF 1979.

SOME AGITATOR SHAFT FAILURES OCCURRED IN THE REACTION TANK CAUSING

KANSAS POWER & LIGHT: LAWRENCE 5 (CONT.)

			TY OPERABILÎTY RE	ELIABILITY	UTILIZATION	% REMOVAL SO2 PART.	PER HOURS	BOILER HOURS	FGD HOURS	CAP.
		# * * * * * * * * * * * * * * * * * * *	MAINTENANCE ATTE							
1/80	SYSTEM	100.0	100.0		100.0		744	744	744	
2/80	SYSTEM		100.0		51.7		696	360	360	
3/80	SYSTEM		100.0		54.8		744	408	408	
	** PROB	BLEMS/SOLUT	IONS/COMMENTS							
			THE FGD SYSTEM O QUARTER OF 1980. FOR TURBINE REPA WAS PERFORMED.	. THE BOI	LER WAS DOWN	FROM MID-FE	BRUARY	TO MID	-MARCH	
4/80	SYSTEM	100.0	100.0	100.0	100.0		720	720	720	
5/80	SYSTEM	100.0	100.0	100.0	80.6		744	600	600	
6/80	SYSTEM	100.0	100.0	100.0	100.0		720	720	720	
	** PROS	BLEMS/SOLUT	IONS/COMMENTS							
			THE BOILER WAS DURING THIS TIME OTHER THAN THIS THE APRIL-JUNE F	GENERAL I	MAINTENANCE W	AS PERFORME	וד אס ס	HE FGD	SYSTEM	•
7/80	SYSTEM	100.0	100.0	100.0	96.1		744	715	715	54.0
	** FRO	BLEMS/SOLUT	IONS/COMMENTS							
			A 29 HOUR OUTAGE BOILER. NO FGD						IN THE	
8/80	SYSTEM	100.0	100.0	100.0	81.5		744	606	606	43.3
	** PRO	BLEMS/SOLUT	IONS/COMMENTS							
			THE OUTAGE TIME PREHEATER TUBE.	IN AUGUST	WAS DUE TO N	ECESSARY RE	PAIR O	F A BOI	LER AI	₹
9/80	SYSTEM	100.0	100.0	100.0	95.7		720	689	689	38.7
	** PROS	BLEMS/SOLUT	IONS/COMMENTS							
			THE BOILER WAS (INSPECTION.	OUT OF SER	VICE FOR APPR	OXIMATELY 3	1 HOUR	S FOR A	SCHED	ULED
10/80	SYSTEM	100.0	100.0	100.0	65.2		744	485	485	
	** PRO	BLEMS/SOLUT	IONS/COMMENTS							
			DURING OCTOBER THERE		Y REPORTED TH	NO MAJOR	FGD-R	ELATED	PROBLE	MS
			THE BOILER WAS	DUT OF SER	VICE 259 HOUR	S DUE TO A	SCHEDU	LED INS	PECTIO	N.
11/80	SYSTEM	100.0	100.0	100.0	100.0		720	720	720	
12/80	SYSTEM	100.0	100.0	100.0	100.0		744	744	744	

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

DURING NOVEMBER AND DECEMBER THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS OCCURRED.

 1/81
 SYSTEM
 744

 2/81
 SYSTEM
 672

 3/81
 SYSTEM
 744

** PROBLEMS/SOLUTIONS/COMMENTS

UTILITY REPORTED THAT NO FGD-RELATED OUTAGES OCCURRED THROUGHOUT THE FIRST QUARTER OF 1981.

THE UNIT WAS SHUT DOWN FOR 17-HOURS IN MARCH DUE TO A SUPERHEATER FAILURE.

 4/81
 SYSTEM
 720

 5/81
 SYSTEM
 744

 6/81
 SYSTEM
 720

 7/81
 SYSTEM
 744

 8/81
 SYSTEM
 744

 9/81
 SYSTEM
 720

** PROBLEMS/SOLUTIONS/COMMENTS

LAWRENCE 5 WAS REPORTED TO BE AVAILABLE 100% OF THE TIME DURING THE THIRD QUARTER 1981. NO FGD SYSTEM-RELATED PROBLEMS WERE REPORTED FOR EITHER THE SECOND OR THIRD QUARTERS.

 10/81
 SYSTEM
 744

 11/81
 SYSTEM
 720

 12/81
 SYSTEM
 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT BOILER OPERATIONS WERE NOT CURTAILED OR REDUCED AS A RESULT OF THE FGD SYSTEM DURING THE FOURTH QUARTER 1981.

 1/82
 SYSTEM
 744

 2/82
 SYSTEM
 672

 3/82
 SYSTEM
 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE FIRST QUARTER 1982. SCMETIME DURING THE FIRST AND/OR SECOND QUARTER 1982, THE UNIT WILL BE SHUTDOWN FOR A SCHEDULED 2 WEEK SPRING OUTAGE.

4/82 SYSTEM 720 5/82 SYSTEM 744

KANSAS POWER & LIGHT: LAWRENCE 5 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

6/82 SYSTEM

720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE SECOND QUARTER 1982.

7/82	SYSTEM	744
8/82	SYSTEM	744
9/82	SYSTEM	720
10/82	SYSTEM	744
11/82	SYSTEM	720
12/82	SYSTEM	744
1/83	SYSTEM	744
2/83	SYSTEM	672
3/83	SYSTEM	744

** PROBLEMS/SOLUTIONS/COMMENTS

OVER THE PAST YEAR THE LAWRENCE 4 AND 5 FGD SYSTEMS HAVE OPERATED WITH NO MAJOR PROBLEMS. THERE HAVE BEEN SOME CHRONIC MINOR PROBLEMS WITH SPRAY HEADER PLUGGING. THERE MAY BE SOME MODIFICATIONS PERFORMED AT SOME POINT IN THE FUTURE TO MINIMIZE THE PROBLEM.

THE DOWNSTREAM DUCTWORK IN BOTH THE LAWRENCE 4 AND 5 FGD SYSTEMS HAS BEEN EXPERIENCING CORROSION THAT WILL REQUIRE SOME DEGREE OF REPLACEMENT. THE CORROSION IS NOT RELATED TO CHLORIDES. A TIME TABLE FOR THE REPAIR WORK WAS NOT REPORTED BY THE UTILITY.

4/83	SYSTEM	720
5/83	SYSTEM	744
6/83	SYSTEM	720
7/83	SYSTEM	744
8/83	SYSTEM	744
9/83	SYSTEM	720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED FORCED OUTAGES WERE ENCOUNTERED DURING THE PERIOD OF APRIL THROUGH SEPTEMBER.

THE NEXT UNIT OUTAGE IS SCHEDULED TO BEGIN THE FIRST WEEK OF OCTOBER AND LAST FROM TWO TO THREE WEEKS. DURING THE OUTAGE, THE UTILITY PLANS TO DO SOME TEMPORARY PATCH WORK ON THE ABSORBER OUTLET DUCTING. THIS TEMPORARY PATCH WORK IS HOPED BY THE UTILITY TO LAST THROUGH 1984.

10/83	SYSTEM	744
11/83	SYSTEM	720
12/83	SYSTEM	744

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURING THE FOURTH QUARTER OF 1983. FGD SYSTEM AVAILABILITY WAS 100%.

1/84	SYSTEM	744
2/84	SYSTEM	696
3/84	SYSTEM	744
4/84	SYSTEM	720
5/84	SYSTEM	744
6/84	SYSTEM	720
7/84	SYSTEM	744
8/84	SYSTEM	744
9/84	SYSTEM	720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT OVERALL FGD SYSTEM AVAILABILITY FOR THE FIRST THREE QUARTERS OF 1984 WAS ABOVE 90%. NO MAJOR FGD-RELATED PROBLEMS WERE REPORTED.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

______ KENTUCKY UTILITIES COMPANY NAME GREEN RIVER PLANT NAME 1-3 UNIT NUMBER CENTRAL CITY CITY STATE KENTUCKY REGULATORY CLASSIFICATION 62. (.145 LB/MMBTU) 387. (.900 LB/MMBTU) ****** (****** LB/MMBTU) PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW 264 GROSS UNIT GENERATING CAPACITY - MM NET UNIT GENERATING CAPACITY W/FGD - MW 59 NET UNIT GENERATING CAPACITY WO/FGD - MW 62 EQUIVALENT SCRUBBED CAPACITY - MW 65 ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER BABCOCK & WILCOX BOILER TYPE PULVERIZED COAL 169.88 (360000 ACFM) 404.4 (760 F) 50. BOILER SERVICE LOAD DESIGN BOILER FLUE GAS FLOW - CU.M/S
BOILER FLUE GAS TEMPERATURE - C STACK HEIGHT - M STACK SHELL CARBON STEEL STACK TOP DIAMETER - M 4.9 (16.8 FT) ** FUEL DATA FUEL TYPE COAL BITUMINOUS 26167. (11250 BTU/LB) FUEL GRADE AVERAGE HEAT CONTENT - J/G RANGE HEAT CONTENT - BTU/LB 10900-11600 9.85 8.85~10.85 AVERAGE ASH CONTENT - % RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - %
RANGE MOISTURE CONTENT - %
AVERAGE SULFUR CONTENT - %
AVERAGE SULFUR CONTENT - % 11.00 10.0-12.0 2.23 RANGE SULFUR CONTENT - 2 2 0-2 7 AVERAGE CHLORIDE CONTENT - % ****** RANGE CHLORIDE CONTENT - % ***** *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER 3 NUMBER OF SPARES n TYPE CYCLONE [MULTIPLE] 280/COLLECTOR SUPPLIER WESTERN PREC. DIVISION, JOY INLET FLUE GAS CAPACITY - CU.M/S
INLET FLUE GAS TEMPERATURE C 49.5 (105000 ACFM) 176.7 (350 F) .5 (2. IN-H20) PRESSURE DROP - KPA PARTICLE REMOVAL EFFICENCY -% 80.0 ** ESP NUMBER TYPE NONE ** PARTICLE SCRUBBER NUMBER NUMBER OF SPARES 0 INITIAL START-UP DATE 9/75 GENERIC TYPE VENTURT SPECIFIC TYPE VARIABLE-THROAT/TOP-ENTRY PLUMB BOB TRADE NAME/COMMON NAME N/A SUPPLIER AMERICAN AIR FILTER SHELL GENERIC MATERIAL CARBON STEEL; STAINLESS STEEL SHELL SPECIFIC MATERIAL AISI 1110; AUSTENITIC LINER GENERIC MATERIAL INORGANIC LINER SPECIFIC MATERIAL HYDRAULICALLY-BONDED MORTAR GAS CONTACTING DEVICE TYPE NONE

1

NUMBER OF CONTACTING ZONES

KENTUCKY UTILITIES: GREEN RIVER 1-3 (CONT.)

```
( 2050 GPM)
( 5.7 GAL/1000ACF)
                                             129.1
LIQUID RECIRCULATION RATE - LITER/S
                                               .8
L/G RATIO - LITER/CU.M
                                             1.7 ( 7.0 IN-H20)
169.9 ( 360000 ACFM)
148.9 ( 300 F)
                                                1.7
PRESSURE DROP - KPA
INLET GAS FLOW RATE - CU.M/S
INLET GAS TEMPERATURE - C
PARTICLE REMOVAL EFFICIENCY - %
                                               98.0
```

THROWAWAY PRODUCT

AMERICAN AIR FILTER SARGENT & LUNDY

WET SCRUBBING

FULL SCALE RETROFIT

LIME NONE

*** FGD SYSTEM

** GENERAL DATA SALEABLE PRODUCT/THROWAWAY PRODUCT SO2 REMOVAL MODE

PROCESS TYPE PROCESS ADDITIVES SYSTEM SUPPLIER A-E FIRM DEVELOPMENT LEVEL NEW/RETROFIT UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.50

98.00 UNIT DESIGN SO2 REMOVAL EFFICIENCY - % ENERGY CONSUMPTION - % 4.6 1 CURRENT STATUS 6/76 COMMERCIAL START-UP INITIAL START-UP 9/75 CONTRACT AWARDED 6/73

** DESIGN AND OPERATING PARAMETERS

DESIGN COAL SULFER CONTENT - % 3.80 3.80 25818.6 DESIGN COAL HEAT CONTENT - J/G (11100 BTU/LB) 14.00 DESIGN COAL ASH CONTENT - % OPER. & MAINT. REQUIREMENT - MANHR/DAY 48.0

** QUENCHER/PRESATURATOR

NUMBER 0

** ABSORBER

NUMBER NUMBER OF SPARES GENERIC TYPE SPECIFIC TYPE TRADE NAME/COMMON TYPE SUPPLIER DIMENSIONS - FT SHELL GENERIC MATERIAL SHELL SPECIFIC MATERIAL

SHELL MATERIAL TRADE NAME/COMMON TYPE LINER GENERIC MATERIAL LINER SPECIFIC MATERIAL LINER MATERIAL TRADE NAME/COMMON TYPE

GAS CONTACTING DEVICE TYPE NUMBER OF CONTACTING ZONES LIQUID RECIRCULATION RATE - LITER/S

L/G RATIO - L/CU.M GAS-SIDE PRESSURE DROP - KPA SUPERFICAL GAS VELOCITY - M/SEC INLET GAS FLOW - CU. M/S INLET GAS TEMPERATURE - C 502 REMOVAL EFFICIENCY - %

PARTICLE REMOVAL EFFICENCY - %

** MIST ELIMINATOR

NUMBER OF STAGES

PRE-MIST ELIMINATOR/MIST ELIMINATOR NUMBER PER SYSTEM NUMBER OF SPARES PER SYSTEM NUMBER PER MODULE GENERIC TYPE SPECIFIC TYPE TRADE NAME/COMMON TYPE MANUFACTURER CONFIGURATION

1 0

PACKED TOWER ENTRAINED PACKING MOBILE BED CONTACTOR AMERICAN AIR FILTER 20.0 X 20.0 X 3.0 CARBON STEEL; STAINLESS STEEL AISI 1110; AUSTENITIC N/A; TYPE 316 INORGANIC HYDRAULICALLY-BONDED MORTAR NR

PLASTIC/RUBBER MOBILE BALLS

1
614. (9750 GPM)
3.6 (27.0 GAL/1000 ACF)
.7 (3.0 IN-H20)
3.7 (12.0 FT/S)
142.99 (303000 ACFM)
.4 7 (116 F)

80.0 98.0

PRIMARY COLLECTOR

0 1 CENTRIFUGAL RADIAL VANE RADIAL BAFFLE AMERICAN AIR FILTER HORIZONTAL

1

1

KENTUCKY UTILITIES: GREEN RIVER 1-3 (CONT.)

```
NUMBER OF PASSES PER STAGE
                                                       1
                                                       4.11 (13.5 FT)
7.6 (3.00 IN)
    FREEBOARD DISTANCE - M
    DISTANCE BETWEEN VANES - CM
                                                       7.6
.6
                                                                  ( 2.3 IN-H20)
    PRESSURE DROP - KPA
                                                                 ( 27.5 FT/S)
    SUPERFICAL GAS VELOCITY - M/S
                                                     8.4
                                                STAINLESS STEEL
    CONSTRUCTION MATERIAL GENERIC TYPE
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                  AUSTENITIC
                                                  FRESH
    WASH WATER SOURCE
    WASH FREQUENCY
                                                  CONTINUOUS
                                                              ( 45 GAL/MIN)
                                                       2.8
    WASH RATE - L/S
** REHEATER
                                                   1
    NUMBER
    NUMBER OF SPARES
                                                   0
    NUMBER PER MODULE
                                                   1
                                                  INDIRECT HOT AIR
    GENERIC TYPE
    SPECIFIC TYPE
                                                  EXTERNAL HEAT EXCHANGER
    TRADE NAME/COMMON TYPE
                                                  STEAM TUBE BUNDLE
                                                  22.2
    PERCENT GAS BYPASSED - AVG
   TEMPERATURE INCREASE - C

TEMPERATURE INCREASE - C

INLET FLUE GAS FLOW RATE - CU. M/S

INLET FLUE GAS TEMPERATURE - C

OUTLET FLUE GAS TEMPERATURE - C

CONSTRUCTION MATERIAL GENERIC TYPE

CONSTRUCTION MATERIAL SPECIFIC TYPE

AISI 1110
                                                                  ( 40 F)
                                               142.99 ( 303000 ACFM)
46.7 ( 116 F)
68.9 ( 156 F)
** FANS
    NUMBER
                                                   1
    NUMBER OF SPARES
                                                    0
    DESTGN
                                                   CENTRIFUGAL
    SUPPLIER
                                                   BUFFALO FORGE
    FUNCTION
                                                   BOOSTER
    APPLICATION
                                                   FCRCED DRAFT
    SERVICE
                                                  DRY
                                                 169.88 ( 360000 ACFM)
148.9 ( 300 F)
    FLUE GAS FLOW RATE - CU.M/S
    FLUE GAS TEMPERATURE - C
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                CARBON STEEL
** DAMPERS
   NUMBER
                                                   10
    FUNCTION
                                                   CONTROL
    GENERIC TYPE
                                                   LOUVER
    SPECIFIC TYPE
                                                   NR
    MODULATION
                                                  ND
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                  ИR
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                  NR
    LINER GENERIC MATERIAL TYPE
                                                   NR
    LINER SPECIFIC MATERIAL TYPE
                                                   NΡ
** DAMPERS
    NUMBER
    FUNCTION
                                                   SHUT-OFF
    GENERIC TYPE
                                                   GUILLOTINE
    SPECIFIC TYPE
                                                   TOP-ENTRY GUILLOTINE/SEAL AIR
    MODULATION
                                                   OPEN/CLOSED
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                  CARBON STEEL
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                  AISI 1110
    LINER GENERIC MATERIAL TYPE
                                                  NONE
    LINER SPECIFIC MATERIAL TYPE
** DUCTWORK
    LOCATION
                                                  INLET
    CONFIGURATION
                                                  RECTANGULAR
     SHELL GENERIC MATERIAL TYPE
                                                  CARBON STEEL
     SHELL SPECIFIC MATERIAL TYPE
                                                  AISI 1110
     LINER GENERIC MATERIAL TYPE
                                                  NONE
     LINER SPECIFIC MATERIAL TYPE
                                                  N/A
** DUCTWORK
    LOCATION
                                                   OUTLET
    CONFIGURATION
                                                   CIRCULAR
```

KENTUCKY UTILITIES: GREEN RIVER 1-3 (CONT.)

CARBON STEEL SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE AISI 1110 LINER GENERIC MATERIAL TYPE INORGANIC LINER SPECIFIC MATERIAL TYPE HYDRAULICALLY-BONDED MORTAR

** DUCTWORK

LOCATION CONFIGURATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE

** REAGENT PREPARATION EQUIPMENT

FUNCTION DEVICE DEVICE TYPE NUMBER NUMBER OF SPARES

PRODUCT QUALITY - % SOLIDS

** TANKS

SERVICE ABSORBER RECYCLE REAGENT PREP PRODUCT

** PUMPS

SERVICE SCRUBBER/ABSORBER RECIRCULATION 3 SLURRY TRANSFER POND RETURN BLEED STREAM

** SOLIDS CONCENTRATING/DEWATERING

DEVICE

*** SLUDGE

** TREATMENT METHOD DEVICE

PROPRIETARY PROCESS

** DISPOSAL

NATURE TYPE LOCATION SITE TRANSPORTATION METHOD SITE TREATMENT SITE DIMENSIONS SITE CAPACITY - CU.M SITE SERVICE LIFE - YRS

** PROCESS CONTROL AND INSTRUMENTATION

PROCESS STREAM CHEMICAL PARAMETERS PHYSICAL VARIABLES CONTROL LEVELS MONITOR TYPE MONITOR LOCATION PROCESS CHEMISTRY MODE

** WATER BALANCE WATER LOOP TYPE

MAKEUP HATER ADDITION - LITERS/S

SOURCE OF MAKEUP WATER

RETROFIT DUCT TO FGD BOOSTER FAN

CIRCULAR CARBON STEEL AISI 1110 NONE N/A

SLAKER BATCH

AGITATED TANK

1 ۵ 20.0

MIMBED

1 3

NUMBER

2 2 2

NONE

BLEED N/A

N/A

FINAL POND ON-SITE PIPELINE

CLAY LINING [NATURALLY OCCURRING]

9 ACRES/25 FT

203629 (166.5 ACRE-FT)

REACTION TANK [PH]

S02, PH

GAS FLOW, PRESSURE DROP, PERCENT SOLIDS

PH 5.5-6.0; SOLIDS 10%

UNIFLO

PH-REACTANT TANK; DENSITY METERS-RECYCLE LINE

FEEDBACK

CLOSED

4.7 (75 GPM)

RIVER WATER

KENTUCKY UTILITIES: GREEN RIVER 1-3 (CONT.)

** CHEMICALS AND CONSUMPTION

	ABSORBENT
FUNCTION	MOSUKBENI
NAME 1	LIME
CONSUMPTION	2 TPH
POINT OF ADDITION	SLAKER

** FGD SPARE CAPACITY INDICES

SCRUBBER - %	. U
ABSORBER - %	. 0
MIST ELIMINATOR - %	.0
REHEATER - %	.0
FAN - %	.0
SLAKER - %	.0
EFFLUENT HOLD TANK - %	.0
RECIRCULATION PUMP - %	33.0

** FGD SPARE COMPONENT INDICES

SCRUBBER	.0
ABSCREER	.0
MIST ELIMINATOR	.0
REHEATER	.0
FAN	.0
SLAKER	.0
EFFLUENT HOLD TANK	.0
RECIRCULATION PUMP	1.0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

9/75 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE SYSTEM BECAME OPERATIONAL SEPTEMBER 13, 1975 ON A HALF-LOAD BASIS BECAUSE OF A TURBINE OVERHAUL. LOGGING OF OPERATING DATA BEGAN DECEMBER 1975.

10/75	SYSTEM					744		
11/75	SYSTEM					720		
12/75	SYSTEM	74.0	65.0	78. 0	35.0	744	398	257
1/76	SYSTEM	42.0	11.0	14.0	9.0	744	572	64

** PROBLEMS/SOLUTIONS/COMMENTS

A MAJOR PROBLEM WAS FAILURE OF THE RECYCLE PUMPS.

THAWING AND REPAIR OF NUMEROUS FROZEN LINES WAS REQUIRED.

SHUTDOWN OF SUMP PUMPS WAS NECESSARY.

A MAJOR PROBLEM AREA WAS THE FEED TANK AGITATOR.

2/76 SYSTEM 70.0 42.0 42.0 30.0 696 499 211

** PROBLEMS/SOLUTIONS/COMMENTS

REPAIRS WERE MADE TO THE TANK AGITATORS, SLAKE TANKS AND MIX-HOLD TANKS CONTRIBUTING TO OUTAGE TIME.

REPAIRS AND CLEANOUT OF REACTANT PUMPS CONTRIBUTATED TO OUTAGE TIME.

3/76 SYSTEM 97.0 85.0 95.0 52.0 744 458 386

ERIOD	MODULE		Y OPERABILITY			S02 I			BOILER HOURS		
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS								
			ALL RUBBER-LI	NED IMPELLER	S WERE REPLA	CED IN	THE I	PUMPS.			
4/76	SYSTEM	90.0	100.0	100.0	77.0			720	552	552	
5/76	SYSTEM	81.0	100.0	100.0	61.0			744	456	456	
6/76	SYSTEM	100.0	99.0	99.0	82.0			720	597	589	
7/76	SYSTEM	90.0	98.0	99.0	77.0			744	584	574	
8/76	SYSTEM	97.0	97.0	97.0	97.0			744	744	722	
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS								
			VIBRATION IN SHUTDOWN FOR			FAN NEC	CESSI	TATED A	22 HOU	JR SYST	rem
9/76	SYSTEM	86.0	100.0	100.0	79.0			720	571	571	
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS								
			MINOR FAN PRO	BLEMS OCCURR	ED BUT NO FO	RCED O	JTAGE	TIME N	IAS REQU	JIRED.	
			HALF-LOAD OPE BEARING PROBL								:
0/76	SYSTEM	100.0	100.0	100.0	94.0			744	699	699	
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS								
			MINOR FAN PROE	LEMS OCCURRE	D BUT NO FOR	CED OU	TAGE	TIME W	AS REQUI	IRED.	
			HALF-LOAD OPER BEARING PROBLE							JSE OF	
1/76	SYSTEM	100.0	100.0	98.0	98.0			720	704	704	
2/76	SYSTEM	73.0	97.0	87.0	70.0			744	536	517	
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS								
			DURING NOVEME THE SYSTEM WH AND REPLACED	ILE THE UTIL	ITY CONDUCTE	D A CH	ECKOU	T OF TH	HE SCRU		
1/77	SYSTEM	94.0	94.0	94.0	94.0			744	744	6 98	
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS								
			DURING THE MO	NTH OF JANUA	RY NO PROBLE	MS OCC	URRED				
2/77	SYSTEM	36.0	91.0	91.0	36.0			672	266	243	

** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE MONTH OF FEBRUARY IT WAS FOUND THAT THE CARBOLINE STACK LINER WAS BADLY DETERIORATED. SCRUBBER AND BOILER OPERATIONS WERE TERMINATED UNTIL THE STACK LINING WAS REPAIRED. THE STACK WAS REPAIRED FIRST BY WELDING A BACKUP METAL PLATE TO THE PORTIONS OF THE STACK WHERE PITTING

KENTUCKY UTILITIES: GREEN RIVER 1-3 (CONT.)

3/78 SYSTEM 97.0 .0

				DEDECORMANIC	CF DATA					
PERIOD	MODULE			PERFORMANO RELIABILITY (L PER T. HOURS	BOILER HOURS	FGD HOURS	CAP. FACTOR
ca ca wo cu cu wo wo	C C F F 8 8	_	_	E ENTIRE STACK			A REFRA		OATING	
			HE BOILER IS OR PARTICULA	NOT OPERATED	WITHOUT THE	SCRUBBER	BECAUSE	THERE	IS NO !	ESP
4/77	SYSTEM	40.0	98.0	98. 0	23.0		720	167	164	
5/77	SYSTEM	99.0	98.0	98.0	69.0		744	527	513	
6/77	SYSTEM	100.0	100.0	100.0	5.0		720	34	34	
	** PROB	BLEMS/SOLUTION	NS/COMMENTS							
			_	SCRUBBER MODUL EAKING IN THE		REPAIRS T	O THE UN	DERBED I	DAMPER	
			LIME SLAKING	OPERATIONS WA	AS REPAIRED.					
7/77	SYSTEM	100.0			.0		744	0	0	.0
	** PROBLEMS/SOLUTIONS/COMMENTS									
			· - ·	PLANT OPERATION CH CONTINUED T				ER AND 1	FGD SYS	STEM
8/77	SYSTEM	100.0			.0		744	0	0	.0
9/77	SYSTEM	100.0			.0		720	0	0	.0
10/77	SYSTEM	100.0			.0		744	0	0	.0
11/77	SYSTEM	86.0	91.0	91.0	41.0		720	332	301	
	** PROS	BLEMS/SOLUTIO	NS/COMMENTS							
				E ENCOUNTERED LURES. TWO PI					COATI	NGS
			SUMP PUMP FA	ILURES WERE NO	OTED.					
			LEAKS IN THE	PACKING WERE	NOTED.					
12/77	SYSTEM	50.0	63.0	91.0	50.0		744	596	375	
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS							
			NUMEROUS FRE OUTAGE TIME.	EZE UPS WERE	ENCOUNTERED	DURING DE	CEMBER C	AUSING	FGD SY	STEM
1/78	SYSTEM	31.0	32.0	32.0	23.0		744	537	170	
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS							
				T DOWN AFTER . SED BY THE FR						NUARY.
2/78	SYSTEM	97.0	.0		.0		672	672	0	

. 0

744 669 0

PERFORMANCE DATA	
PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION	% REMOVAL PER BOILER FGD CAP.
	SO2 PART. HOURS HOURS HOURS FACTOR
** PROBLEMS/SOLUTIONS/COMMENTS	

THE SYSTEM COULD HAVE BEEN CONSIDERED AVAILABLE THROUGHOUT MOST OF THE WINTER PERIOD BUT BECAUSE EMERGENCY CONDITIONS THE UTILITY CHOSE TO CONCENTRATE THEIR MAINTENANCE CREWS ON POWER GENERATION RATHER THAN FGD OPERATION. UNDER NORMAL CONDITIONS THE RELATIVELY MINOR FGD SYSTEM PROBLEMS WOULD HAVE BEEN SOLVED MORE QUICKLY.

DURING THE FREEZE UPS NUMEROUS GASKETS WERE TORN THROUGHOUT THE SYSTEM. THE SYSTEM WAS SHUT DOWN COMPLETELY FOR REPAIR WORK DURING FEBRUARY AND MARCH.

4/78	SYSTEM	41.0	99.0	99.0	41.0	720	296	295
5/78	SYSTEM	64.0	100.0	98.0	64.0	744	474	474

** PROBLEMS/SOLUTIONS/COMMENTS

THE SCREENS ON THE SUCTION SIDE OF THE PUMPS THAT PUMP THE SLURRY FROM THE PREP ROOM TO THE NOZZLES EXPERIENCED PLUGGING PROBLEMS. THE SCREENS GET PLUGGED WITH LARGE GRIT IN THE SLURRY AND ARE SUCKED OUT OF POSITION BY THE PUMPS. THE UTILITY REPORTED THAT THIS TENDS TO BE A RECURRING PROBLEM.

6/78	SYSTEM	73.0	100.0	100.0	73.0	720	525	524
7/78	SYSTEM	13.0	96.0	100.0	13.0	744	103	99

** PROBLEMS/SOLUTIONS/COMMENTS

BOILER AND FGD SYSTEM OUTAGES DURING JUNE AND JULY WERE FOR ROUTINE MAINTENANCE.

8/78 SYSTEM	61.0	99.0	99.0	28. 0	744	207	205

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS DOWN FROM AUGUST 1 THROUGH AUGUST 12 AS A RESULT OF BLEED PUMP PROBLEMS.

9/78 SYSTEM 76.0 98.0 100.0 41.0 720 303 298

** PROBLEMS/SOLUTIONS/COMMENTS

BECAUSE OF PLUGGING PROBLEMS THE FGD SYSTEM WAS OPERATED AT APPROXIMATELY ONE THIRD OF TOTAL CAPACITY THE LAST TWO WEEKS OF SEPTEMBER.

10/78 SYSTEM 30.0 94.0 96.0 30.0 744 236 222

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM EXPERIENCED RECYCLE TANK SCREEN PLUGGING.

THE FGD SYSTEM EXPERIENCED VIBRATING FAN PROBLEMS.

11/78 SYSTEM 24.0 100.0 74.0 24.0 720 175 175

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS DOWN THE LAST TWO WEEKS OF NOVEMBER DUE TO LOW LOAD DEMAND.

12/78	SYSTEM	.0			.0	744	0	0	. 0
1/79	SYSTEM	.0	.0	.0	.0	744	1	0	

KENTUCKY UTILITIES: GREEN RIVER 1-3 (CONT.)

PERIOD			TY OPERABILITY	RELIABILITY	UTILIZATION	% REMOVAL SO2 PART.	PER	BOILER	FGD	CAP.
9/79	SYSTEM	. 0			.0		672	٥	0	.0
2, , ,			IONS/COMMENTS					_	·	
	AA FROL	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	THE FGD SYSTEM RESULT OF FREE						RY AS	A
3/79	SYSTEM	11.2	100.0	100.0	11.2		744	83	83	
4/79	SYSTEM	18.2	100.0	100.0	18.2		720	131	131	
	** PROB	BLEMS/SOLUT	IONS/COMMENTS							
			THE LOW OPERAT PROBLEMS.	IONAL HOURS	FOR MARCH AN	D APRIL WER	E DUE	TO RECY	CLE PUT	1P
5/79	SYSTEM	100.0			.0		744	0	0	.0
	** PROE	BLEMS/SOLUT	IONS/COMMENTS							
			THE BOILER WAS THROUGH THE EN SYSTEM WILL BE THIS WAS FOUND	D OF SEPTEM INSTALLED	BER. DURING TO BOOST THE	THIS OUTAGE TEMPERATURE	AN INT	DIRECT :	STEAM F	REHEAT E GAS.
6 /79	SYSTEM	100.0			.0		720	0	0	.0
	** PRO	BLEMS/SOLUT	IONS/COMMENTS							
			THE UNIT REMAINOT EXPECTED T						s. IT	IS
7/79	SYSTEM	100.0			.0		744	0	0	.0
8/79	SYSTEM	100.0			.0		744	0	0	.0
9/79	SYSTEM	100.0			.0		720	0	0	.0
	** PRO	SLEMS/SOLUT	IONS/COMMENTS							
			THE BOILER REM BOILER TEMPERA SUPERHEATERS M	TURE VALVES	AND PIPING B	ETWEEN THE	PRIMAR	Y AND S	ECONDAI	₹Y
			ON LINE UNTIL	THE FIRST O		POSSIBLY A	S LATE		····	
			ON LINE UNTIL THE NEW INDIRE AS THE BOILER	CT REHEAT S	F THE YEAR OR YSTEM IS IN P					S 500H
10/79	SYSTEM	100.0	THE NEW INDIRE	CT REHEAT S	F THE YEAR OR YSTEM IS IN P			R OPERA		
	SYSTEM SYSTEM	100.0 100.0	THE NEW INDIRE	CT REHEAT S	F THE YEAR OR YSTEM IS IN P SERVICE.		ADY FO	R OPERA	TION A	.0
11/79			THE NEW INDIRE	CT REHEAT S	F THE YEAR OR YSTEM IS IN P SERVICE.		ADY FO	R OPERA 0	TION A	.0
11/79	SYSTEM SYSTEM	100.0	THE NEW INDIRE	CT REHEAT S	F THE YEAR OR YSTEM IS IN P SERVICE0 .0		744 720	R OPERA 0	TION A	.0
11/79	SYSTEM SYSTEM	100.0	THE NEW INDIRE AS THE BOILER	CT REHEAT S RETURNS TO UING ON THE MARCH 1980	F THE YEAR OR YSTEM IS IN P SERVICE0 .0 .0 .0 REPAIRS OF T . THE FGD SY	LACE AND RE	744 720 744 ER. T	R OPERA 0 0 0 HE UNIT	TION A 0 0 0 MAY B	.0 .0 .0
11/79	SYSTEM SYSTEM	100.0 100.0 BLEMS/SOLUT	THE NEW INDIRE AS THE BOILER IONS/COMMENTS WORK IS CONTIN SHUT DOWN INTO	CT REHEAT S RETURNS TO UING ON THE MARCH 1980	F THE YEAR OR YSTEM IS IN P SERVICE0 .0 .0 .0 REPAIRS OF T . THE FGD SY	LACE AND RE	744 720 744 ER. T	R OPERA 0 0 0 HE UNITE THROU	TION A 0 0 0 MAY B	.0 .0 .0

PERIOD	MODULE	AVAILABILI	TY OPERABILITY RELIABILITY	UTILIZATION	% REMOVA SO2 PAR				CAP.
3/80	SYSTEM	100.0		. 0		744	0	0	.0
	** PROB	LEMS/SOLUT	IONS/COMMENTS						
			THE BOILER REMAINED OUT OF EXPECTED TO BE OPERATING		TO BOILE	R REPAIRS	. THE	UNIT :	IS
4/8 0	SYSTEM	100.0		.0		720	0	0	.0
5/80	SYSTEM	100.0		.0		744	0	0	.0
6/80	SYSTEM	100.0		.0		720	0	0	.0
	** PROE	BLEMS/SOLUT	IONS/COMMENTS						
			THE FGD SYSTEM REMAINED OF RESULT OF THE ON-GOING BOTH HAS BEEN DELAYED BY THE U	DILER REPAIRS.	COMPLET	ION OF TH	E BOIL		
7/80	SYSTEM	100.0		.0		744	0	0	.0
	** PROE	BLEMS/SOLUT	IONS/COMMENTS						
			THE BOILER REPAIRS HAVE E				LER DI	тои с	
8/80	SYSTEM	100.0		.0		744	0	0	.0
9/80	SYSTEM	100.0		.0		720	0	0	.0
	** PROE	BLEMS/SOLUT	IONS/COMMENTS						
			TURBINE REPAIRS CONTINUED WAS AVAILABLE FOR OPERAT		ST AND SE	PTEMBER.	THE F	GD SYS	TEM
10/80	SYSTEM	100.0		.0		744	0	0	.0
1/80	SYSTEM	100.0		.0		720	0	0	.0
.2/80	SYSTEM	100.0		.0		744	0	0	.0
	** PROE	BLEMS/SOLUT	IONS/COMMENTS						
			DURING THE FOURTH QUARTER RESTART THE BOILER IN MIC BY FAULTY INSULATORS. THE	D-DECEMBER RES	ULTED IN	A BLOWN G	SENERAT	OR CAU	SED
			DURING THE PERIOD THE BO	ILER CONTROL V	ALVES HAD	TO BE RE	PLACED		
			THE FGD SYSTEM WAS AVAIL.	ABLE 100% OF T	HE TIME D	URING THE	FOURT	H QUAR	TER.
1/81	SYSTEM	100.0		.0		744	0	0	.0
2/81	SYSTEM	100.0		.0		672	0	0	.0

** PROBLEMS/SOLUTIONS/COMMENTS

3/81 SYSTEM 100.0

DURING MARCH AN ATTEMPT TO RUN A FULL LOAD COMPLIANCE TEST FAILED DUE TO BLOWN INSULATORS. THE UTILITY IS PRESENTLY WAITING ON NEW INSULATORS.

.0

744 0 0 .0

THE FGD SYSTEM WAS AVAILABLE 100% OF THE TIME DURING THE FIRST QUARTER.

KENTUCKY UTILITIES: GREEN RIVER 1-3 (CONT.)

PERIOD	MODULE	AVAILABILIT	Y OPERABILITY RELIABILITY UTILI		% REMOVAL SO2 PART.	HOURS	BOILER HOURS	FGD HOURS	CAP.
4/81	SYSTEM	100.0		.0		720	0	0	.0
5/81	SYSTEM	100.0		. 0		744	0	0	.0
6/81	SYSTEM	100.0		.0		720	0	0	. 0
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS						
			THE FGD SYSTEM DID NOT OPERATE IS WAITING FOR NEW GENERATOR TE AVAILABLE, HOWEVER, FOR OPERATI	RMINAL					JTILITY
7/81	SYSTEM	100.0		.0		744	0	0	.0
8/81	SYSTEM	100.0		.0		744	0	0	.0
9/81	SYSTEM	100.0		.0		720	0	0	.0
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS						
			THE GREEN RIVER UNITS 1-3 REMAI THE FGD SYSTEM WAS AVAILABLE FO					QUARTE	7 1981.
10/81	SYSTEM	100.0		.0		744	0	0	
11/81	SYSTEM	100.0		.0		720	0	0	
12/81	SYSTEM	100.0		.0		744	0	0	
	** PRO	BLEMS/SOLUTI	CONS/COMMENTS						
			THE BOILER WAS DOWN THROUGHOUT TENDED TO OPERATE THE BOILER FO LIQUID CIRCUITS FROZE DUE TO TH THAWED THE UTILITY NO LONGER RE	R A SHO IE WEATH	RT TIME HOW IER. BY THE	EVER,	THE FGD	SYSTE	1
1/82	SYSTEM	100.0		.0		744	0	0	.0
2/82	SYSTEM	100.0		.0		672	0	0	.0
3/82	SYSTEM	100.0		.0		744	0	0	.0
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS						
			DURING THE FIRST QUARTER THE SY DUE TO A LACK OF POWER DEMAND 1					N; HOW	EVER,
4/82	SYSTEM	100.0		.0		720	0	0	.0
	** PRO	BLEMS/SOLUT	IONS/COMMENTS						
			THE SYSTEM DID NOT OPERATE DURI	NG APR	L DUE TO A	LACK O	F POWER	DEMAN	D.
5/82	SYSTEM	100.0		5.0		744	39	39	
	** PRO	BLEMS/SOLUT:	CONS/COMMENTS						
			DURING MAY THE SYSTEM OPERATED TESTS SCHEDULED FOR JUNE.	APPROXI	MATELY 39 H	OURS I	N PREPA	RATION	FOR
6/82	SYSTEM	100.0	1	14.7		720	106	106	

ERIOD			Y OPERABILITY	RELIABILITY	-	% REMOVAL SO2 PART	. HOURS			CAP. FACTOR
	** 000	RI FMS/SOLUTT	ONS/COMMENTS							
	** 1 ***		DURING JUNE TO			KIMATELY 100	HOURS	IN WHI	CH TIME	Ē
7/82	SYSTEM	100.0	100.0	100.0	8.5		744	63	63	6.9
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS							
			THE SYSTEM OF	ERATED ONLY	63 HOURS DURI	נאס JULY DUI	TO LO	POWER	DEMAN).
8/82	SYSTEM	100.0			.0		744	0	0	.0
9/82	SYSTEM	100.0			.0		720	0	0	.0
10/82	SYSTEM	100.0			.0		744	0	0	.0
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS							
			THE SYSTEM DI	NOT OPERAT	E DURING AUGU	JST, SEPTEM	BER, OR	OCTOBE	R DUE	LO FOM
11/82	SYSTEM	100.0	100.0	100.0	1.5		720	11	11	. 5
	** PRO	BLEMS/SOLUTI	CONS/COMMENTS							
			THE SYSTEM OP	ERATED ONLY	11 HOURS DUR	ING NOVEMBE	R DUE TO	LOW P	OWER DE	EMAND.
12/82	SYSTEM	100.0			.0		744	0	0	.0
1/83	SYSTEM	100.0			.0		744	0	0	.0
2/83	SYSTEM	100.0			.0		672	0	0	.0
3/83	SYSTEM	100.0			.0		744	0	0	.0
	** PRO	BLEMS/SOLUTI	CONS/COMMENTS							
			THE SYSTEM DI 1983 DUE TO L			PERIOD OF	DECEMBER	R 1982	THROUGH	1 MARCH
4/83	SYSTEM	100.0			. 0		720	0	0	.0
5/83	SYSTEM	100.0			.0		744	0	0	.0
6/83	SYSTEM	100.0			.0		720	0	0	.0
	** PRO	BLEMS/SOLUT	CONS/COMMENTS							
			THE UTILITY R QUARTER DUE T			DID NOT OPE	RATE DUI	RING TH	E SECO	4 D
7/83	SYSTEM	100.0	100.0	100.0	34.4		744	256	256	11.1
	** PRO	BLEMS/SOLUTI	CONS/COMMENTS							
			THE UTILITY R	EPORTED THAT	NO MAJOR FG	D-RELATED P	ROBLEMS	WERE E	NCOUNT	ERED
8/83	SYSTEM	97.8	100.0	100.0	87.2		744	649	649	29.9

KENTUCKY UTILITIES: GREEN RIVER 1-3 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS BROUGHT DOWN DURING AUGUST DUE TO LACK OF POWER DEMAND AND REPAIRS WERE MADE ON A LEAKING FLOODED ELBOW PRECEDING THE MOBILE BED CONTACTOR.

9/83 SYSTEM 98.6 100.0 97.1 46.0 720 331 331 12.9

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS DOWN DURING PART OF SEPTEMBER DUE TO THE CONTINUED PROBLEM WITH THE LEAKING FLOODED ELBOW.

10/83	SYSTEM	100.0			.0	744	0	0	.0
11/83	SYSTEM	100.0	100.0	100.0	7.4	720	53	53	2.1
12/83	SYSTEM	100.0			.0	744	0	0	.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE UNIT WAS DOWN DURING MOST OF THE FOURTH QUARTER DUE TO LOW POWER DEMAND.

1/84	SYSTEM	.0	.0	744	0	0	.0
2/84	SYSTEM	.0	.0	696	0	0	.0
3/84	SYSTEM	100.0	. 0	744	0	0	.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE UNITS WERE OFF LINE DURING THE FIRST QUARTER OF 1984 DUE TO LOW POWER DEMAND. IN ADDITION, BECAUSE OF SEVERE WEATHER CONDITIONS AND THE INTERMITTENT MODE OF OPERATION OF THE UNITS, THE FGD SYSTEM WAS NOT AVAILABLE UNTIL MARCH.

4/84	SYSTEM	720
5/84	SYSTEM	744
6/84	SYSTEM	720
7/84	SYSTEM	744
8/84	SYSTEM	744
9/84	SYSTEM	720

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE SECOND AND THIRD QUARTER OF 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COMPANY NAME LAKELAND UTILITIES PLANT NAME MCINTOSH UNIT NUMBER LAKELAND CITY STATE FLORIDA REGULATORY CLASSIFICATION 19. (.044 LB/MMBTU) 516. (1.200 LB/MMBTU) ****** (****** LB/MMBTU) 570 364 PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW
NET UNIT GENERATING CAPACITY W/FGD - MW
NET UNIT GENERATING CAPACITY WO/FGD - MW 350 495 364 FQUIVALENT SCRUBBED CAPACITY - MW ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER BABCOCK & WILCOX BOILER TYPE PULVERIZED COAL BOILER SERVICE LOAD BASE DESIGN BOILER FLUE GAS FLOW - CU.M/S ********
BOILER FLUE GAS TEMPERATURE - C 143.3 (***** ACFM) 143.3 (290 F) 76. (250 FT) CONCRETE STACK HEIGHT - M (250 FT) STACK SHELL STACK TOP DIAMETER - M ***** (**** FT) ** FUEL DATA FUEL TYPE COAL FUEL GRADE BITUMINOUS 26749. (11500 BTU/LB) AVERAGE HEAT CONTENT - J/G RANGE HEAT CONTENT - BTU/LB 11200-13500 AVERAGE ASH CONTENT - % 10.00 7.0-17.0 RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - % 6.00 RANGE MOISTURE CONTENT - % 4.2-9.5 AVERAGE SULFUR CONTENT - % 2.56 RANGE SULFUR CONTENT - X 1.3-3.6 AVERAGE CHLORIDE CONTENT - % .01 0.01-0.14 RANGE CHLORIDE CONTENT - % *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER n TYPE NONE ** FABRIC FILTER NUMBER Λ TYPE NONE ** ESP NUMBER 2 NUMBER OF SPARES COLD SIDE TYPE BABCOCK & WILCOX SUPPLIER 251.9 (533800 ACFM) 138.9 (282 F) INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE - C PARTICLE REMOVAL EFFICENCY - % 99.6 ** PARTICLE SCRUBBER NUMBER 0 GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL N/A N/A LINER GENERIC MATERIAL LINER SPECIFIC MATERIAL N/A GAS CONTACTING DEVICE TYPE N/A

LAKELAND UTILITIES: MCINTOSH 3 (CONT.)

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*** FGD SYSTEM
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** GENERAL DATA
                                              THROWAWAY PRODUCT
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                              WET SCRUBBING
   SO2 REMOVAL MODE
   PROCESS TYPE
                                              LIMESTONE
   PROCESS ADDITIVES
                                              NONE
   SYSTEM SUPPLIER
                                              BABCOCK & WILCOX
   A-E FIRM
                                              C.T. MAIN
   DEVELOPMENT LEVEL
                                              FULL SCALE
   NEW/PETROFIT
                                              NEW
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.60
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                85.00
   CURRENT STATUS
                                               1
   COMMERCIAL START-UP
                                               9/82
   INITIAL START-UP
                                               7/82
   CONTRACT AWARDED
                                               3/78
** DESIGN AND OPERATING PARAMETERS
   SPACE REQUIREMENTS - SQ M
                                              1858.0
                                                           ( 20000 SQ FT)
    OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                               24.0
** QUENCHER/PRESATURATOR
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              NP
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              NR
** ABSORBER
   NUMBER
                                               2
   NUMBER OF SPARES
                                               O
   GENERIC TYPE
                                              SPRAY TOWER
   SPECIFIC TYPE
                                              OPEN COUNTERCURRENT SPRAY
   TRADE NAME/COMMON TYPE
                                              N/A
   SUFPLIER
                                              BABCOCK & WILCOX
   SHELL GENERIC MATERIAL
                                              STAINLESS STEEL
   SHELL SPECIFIC MATERIAL
                                              AUSTENITIC
   SHELL MATERIAL TRADE NAME/COMMON TYPE
                                              NØ
   LINER GENERIC MATERIAL
                                              NONE
   LINER SPECIFIC MATERIAL
                                              N/A
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                              N/A
   GAS CONTACTING DEVICE TYPE
                                              NONE
   NUMBER OF CONTACTING ZONES
                                               2
   LIQUID RECIRCULATION RATE - LITER/S
                                               2520.
                                                           (40000 GPM)
   L/G RATIO - L/CU.M
                                               10.7
                                                            ( 80.0 GAL/1000 ACF)
   GAS-SIDE PRESSURE DROP - KPA
                                                 1.9
                                                            ( 7.5 IN-H20)
   INLET GAS FLOW - CU. M/S
                                               584.64
                                                            (1238898 ACFM)
   INLET GAS TEMPERATURE - C
                                                54.4
                                                            ( 130 F)
   SO2 REMOVAL EFFICIENCY - %
                                                85.0
** MIST ELIMINATOR
   PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                              PRIMARY COLLECTOR
   NUMBER PER SYSTEM
                                              2
   GENERIC TYPE
                                              IMPINGEMENT
   SPECIFIC TYPE
                                              BAFFLE
   TRADE NAME/COMMON TYPE
                                              CLOSED VANE
   CONFIGURATION
                                              HORIZONTAL
   NUMBER OF STAGES
                                                 2
   DISTANCE BETWEEN VANES - CM
                                                114.3
                                                            (45.00 IN)
   PRESSURE DROP - KPA
                                                  .1
                                                            ( .5 IN-H20)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              ORGANIC
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              VINYL ESTER
   WASH EREQUENCY
                                              CONTINUOUS
   WASH RATE L/S
                                                           ( 229 GAL/MIN)
                                                 14.4
** REHEATER
   NUMBER
                                               1
   GENERIC TYPE
                                              INDIRECT HOT AIR
   SPECIFIC TYPE
                                              EXTERNAL HEAT EXCHANGER
   TRADE NAME/COMMON TYPE
                                             STEAM TUBE BUNDLE
                                              22.2 (
   TEMPERATURE INCREASE - C
                                                                40 F)
   INLET FLUE GAS FLOW RATE - CU. M/S
                                                 73.55
                                                           ( 155858 ACFM)
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LAKELAND UTILITIES: MCINTOSH 3 (CONT.) INLET FLUE GAS TEMPERATURE - C (381 F) 193.9 CONSTRUCTION MATERIAL GENERIC TYPE STAINLESS STEEL CONSTRUCTION MATERIAL SPECIFIC TYPE AUSTENITIC ** FANS NUMBER 2 NUMBER OF SPARES 0 DESIGN CENTRIFUGAL SUPPLIER TLT-BABCOCK FUNCTION UNIT **APPLICATION** FORCED DRAFT SERVICE DRY PRESSURE DROP - KPA (20.9 IN-H20) 6.4 CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL ** FANS NUMBER 4 TLT-BABCOCK SUPPLIER ** FANS NUMBER 2 NUMBER OF SPARES 0 DESIGN CENTRIFUGAL SUPPLIER GREEN FAN FUNCTION **BOOSTER** APPLICATION FORCED DRAFT SERVICE DRY PRESSURE DROP - KPA 10.1 (33.1 IN-H20) CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL ** DAMPERS **FUNCTION** NR GENERIC TYPE NR SPECIFIC TYPE ND CONSTRUCTION MATERIAL GENERIC TYPE NR CONSTRUCTION MATERIAL SPECIFIC TYPE ND LINER GENERIC MATERIAL TYPE NΒ LINER SPECIFIC MATERIAL TYPE NP ** DUCTWORK LOCATION ID FAN DISCHARGE TO STACK SHELL GENERIC MATERIAL TYPE CARBON STEEL SHELL SPECIFIC MATERIAL TYPE AISI 1110 LINER GENERIC MATERIAL TYPE ORGANIC LINER SPECIFIC MATERIAL TYPE INERT FLAKE-FILLED VINYL ESTER ** DUCTWORK 2 BYPASS STREAMS LOCATION SHELL GENERIC MATERIAL TYPE CARBON STEEL SHELL SPECIFIC MATERIAL TYPE AISI 1110 LINER GENERIC MATERIAL TYPE INORGANIC LINER SPECIFIC MATERIAL TYPE HYDRAULICALLY-BONDED MORTAR ** REAGENT PREPARATION EQUIPMENT WET BALL MILL FUNCTION DEVICE COMPARTMENTED DEVICE TYPE NR NUMBER 13.6 (15 TPH) FULL LOAD DRY FEED CAPACITY - M.TONS/HR ** TANKS SERVICE NUMBER _____ ABSORBER RECYCLE 2

QUENCHER

THICKENER OVERFLOW

2

1

LAKELAND UTILITIES: MCINTOSH 3 (CONT.)

ABSORBER

** PUMPS NUMBER SERVICE ----A ABSORBER RECIRCULATION 4 QUENCHER RECIRCULATION 2 CLARIFIED RECIRCULATION WATER ** SOLIDS CONCENTRATING/DEWATERING VACUUM FILTER DEVICE NUMBER 3 0 NUMBER OF SPARES 1080 TON/DAY CAPACITY FEED STREAM CHARACTERISTICS 30% SOLIDS 55% SOLIDS OUTLET STREAM CHARACTERISTICS ** SOLIDS CONCENTRATING/DEWATERING THICKENER DEVICE NUMBER 1 NUMBER OF SPARES 0 CIRCULAR CONFIGURATION 140.0 DIA DIMENSIONS - FT CARBON STEEL SHELL GENERIC MATERIAL TYPE 15% SOLIDS 30% SOLIDS FEED STREAM CHARACTERISTICS OUTLET STREAM CHARACTERISTICS *** SLUDGE FULL LOAD SLUDGE QUANTITY - M.TONS/HR (DRY) 28.8 (31.7 TPH) ** TREATMENT METHOD FIXATION PUG MILL DEVICE PROPRIETARY PROCESS CONVERSION SYSTEMS [POZ-O-TEC] INLET QUALITY - % 55.0 ** DISPOSAL NATURE FINAL TYPE LANDFILL LOCATION ON-SITE SITE TRANSPORTATION METHOD TRUCK SITE TREATMENT NONE SITE DIMENSIONS 125 ACRES X 40 FT SITE CAPACITY CU.M 6115000 (5000.0 ACRE-FT) SITE SERVICE LIFE - YRS 30 ** PROCESS CONTROL AND INSTRUMENTATION CHEMICAL PARAMETERS PH, DENSITY, GAS FLOW, SO2 CONTROL LEVELS PH 5.5-6.0 PROCESS CONTROL MANNER AUTOMATIC PROCESS CHEMISTRY MODE FEED FORWARD ** WATER BALANCE WATER LOOP TYPE CLOSED EVAFORATION WATER LOSS - LITER/S 20.3 (322 GPM) POND SEEPAGE/RUNOFF WATER LOSS - LITERS/S 303 MAKEUP WATER ADDITION - LITERS/S 14.4 (228 GPM) ** CHEMICALS AND CONSUMPTION FUNCTION ABSORBENT NAME LIMESTONE PRINCIPAL CONSTITUENT CACO3 CONSUMPTION 96000 TONS/YR ** FGD SPARE CAPACITY INDICES ABSORBER - % .0 ** FGD SPARE COMPONENT INDICES

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LAKELAND UTILITIES: MCINTOSH 3 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

7/82 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

INITIAL FGD OPERATIONS BEGAN AT THIS FACILITY DURING JULY. THE SYSTEM IS CURRENTLY UNDERGOING SHAKEDOWN/DEBUGGING OPERATIONS.

8/82 SYSTEM 744

9/82 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE MCINTOSH 3 UNIT (BOILER AND FGD SYSTEM) COMMENCED COMMERICAL OPERATION ON SEPTEMBER 1, 1982.

10/82 SYSTEM 744

11/82 SYSTEM 720

12/82 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE FOURTH QUARTER 1982.

1/83 SYSTEM 744

2/83 SYSTEM 672

3/83 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT IT WAS PLEASED WITH THE OPERATION OF THE UNIT AND FGD SYSTEM. THE FGD SYSTEM AVAILABILITY IS REPORTED TO BE GREATER THAN 95%.

NOTE: IN ADDITION TO HAVING THE CAPABILITY OF BURNING APPROXIMATELY 140 TONS/HR OF BITUMINOUS COAL WITH ASH CONTENTS RANGING FROM 7 TO 17 %, THE BOILER IS ALSO DESIGNED TO BURN REFUSE DERIVED FUEL (RDF). THE UNIT IS CURRENTLY BURNING 300 TONS/DAY OF RDF COLLECTED FROM THE NEARBY CITY OF LAKELAND, FLORIDA. THE RDF IS CONSUMED NORMALLY WITHIN ONE 8 HOUR SHIFT. THE REPORTED HEAT CONTENT OF THE RDF IS APPROXIMATELY 5000 BTU/LB COMPARED TO THE AVERAGE 11500 BTU/LB FOR THE COAL. THE RDF PLANT AND BOILER HAVE THE CAPACITY OF BURNING AN ADDITIONAL 8 TO 12 HOURS OF RDF (300 TO 450 TONS). THE UTILITY

CURRENTLY RECEIVES \$6/TON FOR RDF DISPOSAL.

 4/83
 SYSTEM
 720

 5/83
 SYSTEM
 744

 6/83
 SYSTEM
 720

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE PERIOD OF APRIL THROUGH JUNE, 1983.

7/83	NORTH	100.0	100.0	100.0	97.3			
	SOUTH	77.3	79.3	100.0	78. 9			
	SYSTEM	100.0	89.7	100.0	87.3	744	724	655 83.0

LAKELAND UTILITIES: MCINTOSH 3 (CONT.)

802 PART. HOURS HOURS F 8/83 NORTH 100.0 100.0 100.0 78.9 SOUTH 77.3 79.3 100.0 78.9 SYSTEM 100.0 89.7 100.0 87.3 744 724 655 9/83 NORTH 100.0 100.0 100.0 97.3 SOUTH 77.3 79.3 100.0 78.9 SYSTEM 100.0 89.7 100.0 87.3 720 701 634 ** PROBLEHS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO HAJOR FSO-RELATED PROBLEMS MERE ENCOUNTER DURING THE PERIOD OF JULY THROUGH SEPTEMBER 1983. 10/83 NORTH 56.5 100.0 100.0 46.4 SYSTEM 51.5 91.0 100.0 56.5 SOUTH 46.4 82.0 100.0 46.4 SYSTEM 51.5 91.0 100.0 51.4 720 407 370 12/83 NORTH 56.5 100.0 100.0 56.5 SOUTH 46.4 82.1 100.0 44.4 SYSTEM 51.4 91.0 100.0 51.4 720 407 370 12/83 NORTH 56.5 100.0 100.0 56.5 SOUTH 46.4 82.0 100.0 46.4 SYSTEM 51.5 91.0 100.0 51.4 720 407 370 12/83 NORTH 56.5 100.0 100.0 56.5 SOUTH 46.4 82.0 100.0 46.4 SYSTEM 51.5 91.0 100.0 51.5 744 421 383 ** PROBLEHS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGG-RELATED PROBLEMS MERE ENCOUNTER DURING THE FOURTH QUARTER OF 1983. 1/84 SOUTH 100.0 100.0 100.0 100.0 744 744 744 NORTH SYSTEM 100.0 100.0 100.0 19.4 NORTH SYSTEM 100.0 100.0 100.0 100.0	DEDIOD	MODIII E		OPERABLITY							FGD	CAP.
SOUTH	PERIOD	HODULE	AVAILABILIT	OFERADIEIT	KELINDIEI	OTTELEXTEDIT						
SOUTH 100.0 89.7 100.0 77.9	=										*****	
SOUTH	8/83	NORTH	100.0	100.0	100.0	97.3						
SYSTEM 100.0 89.7 100.0 87.3 744 724 655 9/83 NORTH 100.0 100.0 100.0 97.3				79. 3	100.0	78.9						
SOUTH				89.7	100.0	87.3			744	724	655	83.0
SOUTH	9/83	иорти	100.0	100.0	100.0	97.3						
## PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGO-RELATED PROBLEMS HERE ENCOUNTER DURING THE PERIOD OF JULY THROUGH SEPTEMBER 1983. 10/83 NORTH 56.5 100.0 100.0 56.5 50UTH 46.4 82.0 100.0 51.5 744 421 383 11/83 NORTH 56.5 91.0 100.0 51.5 744 421 383 11/83 NORTH 56.5 100.0 100.0 51.5 744 421 383 11/83 NORTH 46.4 82.1 100.0 46.4 575TEM 51.4 91.0 100.0 51.4 720 407 370 12/83 NORTH 46.4 82.0 100.0 51.4 720 407 370 12/83 NORTH 56.5 100.0 100.0 56.5 50UTH 46.4 82.0 100.0 46.4 575TEM 51.5 91.0 100.0 51.5 744 421 383 11/83 NORTH 50.5 91.0 100.0 51.5 744 421 383 11/83 NORTH 50.5 91.0 100.0 100.0 51.5 744 421 383 11/83 NORTH 50.5 91.0 100.0	77 0 3			79 3								
## PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS HERE ENCOUNTER DURING THE PERIOD OF JULY THROUGH SEPTEMBER 1983. 10/83 NORTH 56.5 100.0 100.0 56.5 50UTH 46.4 82.0 100.0 46.4 5YSTEM 51.5 91.0 100.0 51.5 744 421 383 11/83 NORTH 56.5 100.0 100.0 51.5 744 421 383 11/83 NORTH 46.4 82.1 100.0 56.5 50UTH 46.4 82.1 100.0 51.4 720 407 370 12/83 NORTH 46.4 82.0 100.0 51.4 720 407 370 12/83 NORTH 56.5 100.0 100.0 56.5 744 421 383 ### PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTER DURING THE FOURTH QUARTER OF 1983. 1/84 SOUTH 100.0 100.0 100.0 100.0 100.0 744 744 744 744 744 821 837 83 83 83 83 83 83 83 83 83 83 83 83 83						87. 3			720	701	634	83.0
DURING THE PERIOD OF JULY THROUGH SEPTEMBER 1983.		** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
SOUTH 100.0 100.										WERE E	NCOUNTE	ERED
SOUTH 100.0 100.	70/07	MODELL	F/ F	300.0	100.0	E4 E						
SYSTEM	10/83					50.5						
11/83 NORTH			46.4						744	603	707	
SCUTH		SISIEM	51.5	91.0	100.0	51.5			744	421	282	69.4
SYSTEM	11/83	NORTH	56.5	100.0	100.0							
12/83 NOPTH 56.5 100.0 100.0 56.5 SOUTH 46.4 82.0 100.0 46.4 SYSTEM 51.5 91.0 100.0 51.5 744 421 383 *** PROBLEMS/SOLUTIONS/COMMENTS* THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTER DURING THE FOURTH QUARTER OF 1983. 1/84 SOUTH 100.0 100.0 100.0 100.0 744 744 744 744 744 744 744 8 SOUTH 100.0 100.0 100.0 100.0 44.8 696 264 312 364 SOUTH 19.4 100.0 100.0 100.0 19.4 744 144 144 *** PROBLEMS/SOLUTIONS/COMMENTS* *** PROBLEMS/SOLUTIONS/COMMENTS* *** PROBLEMS/SOLUTIONS/COMMENTS* THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS AROSE DURING ASSETTIONS/COMMENTS* *** PROBLEMS/SOLUTIONS/COMMENTS* THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS AROSE DURING ASSETTIONS/COMMENTS* *** PROBLEMS/SOLUTIONS/COMMENTS** THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS AROSE DURING ASSETTIONS/COMMENTS* *** PROBLEMS/SOLUTIONS/COMMENTS** *** PROB		SCUTH			_							
SOUTH		SYSTEM	51.4	91.0	100.0	51.4			720	407	370	69.4
SOUTH	12/83	нтчси	56.5	100.0	100.0	56.5						
*** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTER DURING THE FOURTH QUARTER OF 1983. 1/84 SOUTH 100.0 100.0 100.0 100.0 744 744 744 744 2/84 SOUTH 100.0 100.0 100.0 44.8 696 264 312 748 3/84 SOUTH 19.4 100.0 100.0 19.4 696 264 312 748 *** PROBLEMS/SOLUTIONS/COMMENTS *** PROBLEMS/SOLUTIONS/COMMENTS *** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS AROSE DURING AS 100.1 100.		SOUTH	46.4	82.0								
THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTER DURING THE FOURTH QUARTER OF 1983. 1/84 SOUTH 100.0 100.0 100.0 100.0 744 744 744 744 744 744 744 744 744 74		SYSTEM	51.5	91.0	100.0	51.5			744	421	383	69.4
1/84 SOUTH 100.0 100.0 100.0 100.0 100.0 744		** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
1/84 SOUTH 100.0 100.0 100.0 100.0 744 744 744 744 744 SOUTH 100.0 100.0 100.0 100.0 19.4 744 144 144			Т	HE UTILITY R	EPORTED THAT	NO MAJOR FG	D-RELA	TED PR	OBLEMS	WERE E	NCOUNT	ERED
NORTH SYSTEM 100.0 100.0 100.0 100.0 744 744 744 2/84 SOUTH 100.0 100.0 100.0 44.8 NORTH SYSTEM 100.0 100.0 100.0 44.8 3/84 SOUTH 19.4 100.0 100.0 19.4 NORTH SYSTEM 19.4 100.0 100.0 19.4 *** PROBLEMS/SOLUTIONS/COMMENTS *** THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS AROSE DURING AROSE DURIN			D	URING THE FO	URTH QUARTER	OF 1983.						
2/84 SOUTH 100.0 100.0 100.0 44.8 696 264 312 STEEM 100.0 100.0 100.0 44.8 696 264 312 STEEM 100.0 100.0 100.0 19.4 744 144 144 144 144 144 144 144 144 14	1/84	_	100.0	100.0	100.0	100.0						
NORTH SYSTEM 100.0 100.0 100.0 44.8 696 264 312 3/84 SOUTH 19.4 100.0 100.0 19.4 744 1		SYSTEM	100.0	100.0	100.0	100.0			744	744	744	87.3
SYSTEM 100.0 100.0 100.0 44.8 696 264 312 318	2/84		100.0	100.0	100.0	44.8						
NORTH			100.0	100.0	100.0	44.8			696	264	312	25.8
SYSTEM 19.4 100.0 100.0 19.4 744 144 144 *** PROBLEMS/SOLUTIONS/COMMENTS NO MAJOR FGD RELATED PROBLEMS WERE REPORTED DURING THE FIRST THREE GUARTERS OF 1984. 4/84 SOUTH 100.0 100.0 101.8 98.4 720 696 *** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS AROSE DURING AS NORTH NORTH 96.8 100.0 102.4 95.8	3/84		19.4	100.0	100.0	19.4						
NO MAJOR FGD RELATED PROBLEMS WERE REPORTED DURING THE FIRST THREE 4/84 SOUTH 100.0 100.0 101.8 98.4 NORTH SYSTEM 720 696 ** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS AROSE DURING AS NORTH NORTH NORTH NORTH		SYSTEM	19.4	100.0	100.0	19.4			744	144	144	8.5
QUARTERS OF 1984. 4/84 SOUTH 100.0 100.0 101.8 98.4 NORTH SYSTEM 720 696 ** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS AROSE DURING AS NORTH 5/84 SOUTH 96.8 100.0 102.4 95.8		** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
NORTH SYSTEM 720 696 ** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS AROSE DURING A 5/84 SOUTH 96.8 100.0 102.4 95.8 NORTH						LEMS WERE RE	PORTED	DURIN	G THE	FIRST T	HREE	
NORTH SYSTEM 720 696 ** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS AROSE DURING A 5/84 SOUTH 96.8 100.0 102.4 95.8 NORTH	4/84	SOUTH	100.0	100.0	101.8	98.4						
THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS AROSE DURING A SOUTH 96.8 100.0 102.4 95.8 NORTH									720	696		78.0
5/84 SOUTH 96.8 100.0 102.4 95.8 NORTH		** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
NORTH			т	HE UTILITY R	EPORTED THAT	NO MAJOR FG	D-RELA	TED PR	OB LEMS	AROSE	DURING	APRIL.
	5/84		96.8	100.0	102.4	95.8						
SYSTEM 96.8 100.0 100.0 95.8 744 696 713		SYSTEM	96.8	100.0	100.0	95.8			744	696	713	75.6

LAKELAND UTILITIES: MCINTOSH 3 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS AROSE DURING MAY.

6/84 SOUTH 100.0 100.0 102.6 99.2 NORTH SYSTEM 100.0 100.0 100.0 99.2 720 672 714 74.5

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS AROSE DURING JUNE.

NORTH MODULE DATA WAS NOT REPORTED DURING THE FIRST TWO QUARTERS OF 1984 DUE TO SUSPECTED PROBLEMS WITH AN ELAPSED TIME METER.

7/84 SYSTEM 744 8/84 SYSTEM 744 9/84 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE THIRD QUARTER OF 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

LOUISVILLE GAS & ELECTRIC COMPANY NAME CANE RUN PLANT NAME UNIT NUMBER LOUISVILLE CITY KENTUCKY STATE 50. (.116 LB/MMBTU) 516. (1.200 LB/MMBTU) ****** (****** LB/MMBTU) 992 REGULATORY CLASSIFICATION PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW NET UNIT GENERATING CAPACITY W/FGD - MW 188 175 178 188 NET UNIT GENERATING CAPACITY WO/FGD - MW EQUIVALENT SCRUBBED CAPACITY - MW ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER COMBUSTION ENGINEERING 346.37 (734000 ACFM) 160.0 (320 F) 76. (250 FT) CONCRETE 5.8 BOILER TYPE BOILER SERVICE LOAD DESIGN BOILER FLUE GAS FLOW - CU.M/S
BOILER FLUE GAS TEMPERATURE - C STACK HEIGHT - M STACK SHELL STACK TOP DIAMETER - M ** FUEL DATA FUEL TYPE COAT FUEL GRADE BITUMINOUS AVERAGE HEAT CONTENT - J/G 26284. (11300 BTU/LB) RANGE HEAT CONTENT - BTU/LB 10400-11900 AVERAGE ASH CONTENT - % 15.00 RANGE ASH CONTENT - % 10.0-20.0 AVERAGE MOISTURE CONTENT - % 9.00 RANGE MOISTURE CONTENT - % 8.0-10.8 AVERAGE SULFUR CONTENT - % 3.87 RANGE SULFUR CONTENT - % 3.5-4.0 AVERAGE CHLORIDE CONTENT - % .04 RANGE CHLORIDE CONTENT - % 0.03-0.06 *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER 0 TYPE NONE ** ESP NUMBER 2 NUMBER OF SPARES TYPE COLD SIDE SUPPLIER. RESEARCH-COTTRELL INLET FLUE GAS CAPACITY - CU.M/S 172.2 (365000 ACFM)
INLET FLUE GAS TEMPERATURE - C 160.0 (320 F)
PRESSURE DROP - KPA .0 (0. IN-H20) .0 PARTICLE REMOVAL EFFICENCY - % ** PARTICLE SCRUBBER NUMBER 0 GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL N/A LINER GENERIC MATERIAL N/A LINER SPECIFIC MATERIAL N/A GAS CONTACTING DEVICE TYPE N/A

*** FGD SYSTEM

```
** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                               THROWAWAY PRODUCT
   SO2 REMOVAL MODE
                                               WET SCRUBBING
   PROCESS TYPE
                                               LIME
   PROCESS ADDITIVES
                                               NONE
   SYSTEM SUPPLIER
                                               AMERICAN AIR FILTER
   A-E FIRM
                                               FLUOR - PIONEER
   DEVELOPMENT LEVEL
                                               FULL SCALE
   NEW/RETROFIT
                                               RETROETT
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.00
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                  85.00
   FNERGY CONSUMPTION - %
                                                  1.6
   CURRENT STATUS
                                                1
   COMMERCIAL START-UP
                                                8/77
   INITIAL START-UP
                                                8/76
   CONTRACT AWARDED
                                                4/74
** DESIGN AND OPERATING PARAMETERS
   DESIGN COAL SULFER CONTENT - X
                                                  4.00
   DESIGN COAL HEAT CONTENT - J/G
                                               25586.0
                                                              ( 11000 BTU/LB)
   DESIGN COAL ASH CONTENT - %
                                                 15.00
   DESIGN MOISTURE CONTENT - %
                                                  12.00
   DESIGN CHLORIDE CONTENT - X
                                                   .07
   OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                304.0
** QUENCHER/PRESATURATOR
   NUMBER
   TYPE
                                               WETTED WALL CONICAL FRUSTUM
                                               AMERICAN AIR FILTER
   SUPPLIER.
   INLET GAS FLOW - CU. M/S
                                                 172.24 ( 365000 ACFM)
   INLET GAS TEMPERATURE - C
                                                              ( 320 F)
                                                 160.0
   PRESSURE DROP - KPA
                                                   . 5
                                                             ( 2.0 IN-H20)
                                                             ( 1760 GPM)
   LIQUID RECIRCULATION RATE - LITERS/S
                                                 111.
    L/G RATIO - L/CU. M
                                                              ( 4.8 GAL/1000 ACFM)
                                                    - 6
                                               CARBON STEEL
   CONSTRUCTION MATERIAL GENERIC TYPE
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              AISI 1110
** ABSORBER
                                                2
   NUMBER
   NUMBER OF SPARES
                                                0
                                               PACKED TOWER
   GENERIC TYPE
                                               ENTRAINED PACKING
    SPECIFIC TYPE
                                               MOBILE BED CONTACTOR
   TRADE NAME/COMMON TYPE
                                               AMERICAN AIR FILTER
    SUPPLIER
                                               20.0 X 20.0 X 27.5
   DIMENSIONS - FT
                                               CARBON STEEL
    SHELL GENERIC MATERIAL
    SHELL SPECIFIC MATERIAL
                                               AISI 1110
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                               N/A
                                               INORGANIC; ORGANIC
    LINER GENERIC MATERIAL
    LINER SPECIFIC MATERIAL
                                               HYDRAULICALLY-BONDED MORTAR; INERT FLAKE-FILLED
                                               PRE-KRETE G-8; PLASITE
    LINER MATERIAL TRADE NAME/COMMON TYPE
    GAS CONTACTING DEVICE TYPE
                                               PLASTIC/RUBBER MOBILE BALLS
   NUMBER OF CONTACTING ZONES
                                                1
   LIQUID RECIRCULATION RATE - LITER/S
                                                1110.
                                                              (17625 GPM)
                                                              ( 60.5 GAL/1000 ACF)
    L/G RATIO - L/CU.M
                                                   8.1
   GAS-SIDE PRESSURE DROP - KPA
                                                   1.5
                                                              ( 6.0 IN-H20)
   SUPERFICAL GAS VELOCITY - M/SEC
                                                  3.7
                                                              ( 12.0 FT/S)
   INLET GAS FLOW - CU. M/S
                                                              ( 291500 ACFM)
                                                 137.56
   INLET GAS TEMPERATURE - C
                                                  54.4
                                                              ( 130 F)
   SO2 REMOVAL EFFICIENCY - %
                                                  87.0
** MIST ELIMINATOR
   PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                               PRIMARY COLLECTOR
   NUMBER PER SYSTEM
                                                2
   NUMBER OF SPARES PER SYSTEM
                                                0
   NUMBER PER MODULE
                                               1
   GENERIC TYPE
                                               IMPINGEMENT
   SFECIFIC TYPE
                                               BAFFLE
   TRADE NAME/COMMON TYPE
                                               CLOSED VANE
   CONFIGURATION
                                               HORIZONTAL
```

IOUISVILLE GAS & ELECTRIC: CANE RUN 4 (CONT.)

```
2
   NUMBER OF STAGES
   NUMBER OF PASSES PER STAGE
                                                   3
                                                   1.83
                                                             ( 6.0 FT)
   FREEBOARD DISTANCE - M
                                                             ( 1.20 IN)
   DISTANCE BETWEEN VANES - CM
                                                   3.0
                                                   . 3
                                                             ( 1.2 IN-H20)
   PRESSURE DROP - KPA
                                                             ( 12.0 FT/S)
   SUPERFICAL GAS VELOCITY - M/S
                                                   3.7
   CONSTRUCTION MATERIAL GENERIC TYPE
                                               ORGANIC
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              FIBER-REINFORCED POLYESTER
                                               FRESH
   WASH WATER SOURCE
                                               EVERY 16 MIN.
   WASH FREQUENCY
   WASH RATE - L/S
                                                  5.0
                                                            ( 80 GAL/MIN)
** REHEATER
                                               2
   NUMBER
   NUMBER OF SPARES
                                               0
   NUMBER PER MODULE
                                               1
   GENERIC TYPE
                                              DIRECT COMBUSTION
   SPECIFIC TYPE
                                               EXTERNAL COMBUSTION CHAMBER
    TRADE NAME/COMMON TYPE
                                               OIL
    PERCENT GAS BYPASSED - AVG
                                                    .0
    TEMPERATURE INCREASE - C
                                                 16.7
                                                             ( 30 F)
    INLET FLUE GAS FLOW RATE - CU. M/S
                                               137.56
                                                             ( 291500 ACFM)
                                                             ( 130 F)
( 160 F)
    INLET FLUE GAS TEMPERATURE - C
                                                 54.4
    OUTLET FLUE GAS TEMPERATURE - C
                                                 71.1
   CONSTRUCTION MATERIAL GENERIC TYPE
                                               CAST IRON
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              NR
** FANS
   NUMBER
                                               2
   NUMBER OF SPARES
                                               0
   DESIGN
                                               CENTRIFUGAL
    SUPPLIER
                                               AMERICAN STANDARD
    FUNCTION
                                               BOOSTER
                                               FORCED DRAFT
    APPLICATION
    SERVICE
                                               DRY
    FLUE GAS FLOW RATE - CU.M/S
                                               173.19
                                                             ( 367000 ACFM)
   FLUE GAS TEMPERATURE - C
                                                162.8
                                                             ( 325 F)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                              CARBON STEEL
** FANS
   NUMBER
                                                2
   NUMBER OF SPARES
                                               n
   DESTON
                                               CENTRIFUGAL
    SUPPLIER
                                               BUFFALO FORGE
    FUNCTION
                                               BOOSTER
    APPLICATION
                                               FORCED DRAFT
    SERVICE
                                               DRY
    FLUE GAS FLOW RATE - CU.M/S
                                               173.19
                                                            ( 367000 ACFM)
    FLUE GAS TEMPERATURE - C
                                                162.8
                                                             ( 325 F)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL
** DAMPERS
   NUMBER
                                               20
   FUNCTION
                                               CONTROL
    GENERIC TYPE
                                               LOUVER
    SPECIFIC TYPE
    MANUFACTURER
                                               AMERICAN AIR FILTER
    MODULATION
                                               NP
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               NR
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               NR
    LINER GENERIC MATERIAL TYPE
                                               NR
   LINER SPECIFIC MATERIAL TYPE
                                               NR
** DAMPERS
   NUMBER
   FUNCTION
                                               SHUT-OFF
   GENERIC TYPE
                                               GUILLOTINE
    SPECIFIC TYPE
                                               TOP-ENTRY GUILLOTINE/SEAL AIR
   MANUFACTURER
                                               AMERICAN AIR FILTER
   MODULATION
                                               OPEN/CLOSED
   CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL
```

LOUISVILLE GAS & ELECTRIC: CANE RUN 4 (CONT.)

CONSTRUCTION MATERIAL SPECIFIC TYPE AISI 1110
LINER GENERIC MATERIAL TYPE NR
LINER SPECIFIC MATERIAL TYPE NR

** DAMPERS

FUNCTION
GENERIC TYPE
SPECIFIC TYPE
MANUFACTURER
MODULATION
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
LINER GENERIC MATERIAL TYPE

LINER SPECIFIC MATERIAL TYPE

2
SHUT-OFF
GUILLOTINE
TOP-ENTRY GUILLOTINE/SEAL AIR
AMERICAN AIR FILTER
OPEN/CLOSED
CARBON STEEL
AISI 1110
NONE
N/A

** DAMPERS

NUMBER
FUNCTION
GENERIC TYPE
SPECIFIC TYPE
MANUFACTURER
MODULATION
CONSTRUCTION 1

MODULATION

CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

2
SHUT-OFF
GUILLOTINE
TOP-ENTRY GUILLOTINE/SEAL AIR
AMERICAN AIR FILTER
OPEN/CLOSED
CARBON STEEL
AISI 1110
NR
NR

** DUCTWORK LOCATION

SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE SCRUBBER INLET CARBON STEEL AISI 1110 NONE N/A

** DUCTWORK

LOCATION
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

SCRUBBER OUTLET TO REHEATER
CARBON STEEL
AISI 1110
ORGANIC
INERT FLAKE-FILLED VINYL ESTER

** DUCTWORK

LOCATION
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

OUTLET FROM REHEATER TO STACK CARBON STEEL AISI 1110 INORGANIC HYDRAULICALLY-BONDED MORTAR

** DUCTHORK
LOCATION

SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SFECIFIC MATERIAL TYPE BYPASS CARBON STEEL AISI 1110 NONE N/A

** REAGENT PREPARATION EQUIPMENT

FUNCTION
DEVICE
DEVICE TYPE
NUMBER
NUMBER OF SPARES
PRODUCT QUALITY - % SOLIDS

GRINDING OF SOLIDS FOUND IN BARGE DELIVERED CARB
BALL MILL
TUBE MILL
1
0
25.0

** TANKS

SERVICE
----ABSORBER RECYCLE
LIME SLURRY HOLD TANK
RECYCLE

NUMBER -----2 1 1

LOUISVILLE GAS & ELECTRIC: CANE RUN 4 (CONT.)

PROCESS CHEMISTRY MODE

** PUMPS NUMBER SERVICE -----6 ABSORBER RECIRCULATION 2 THICKENER UNDERFLOW THICKENER OVERFLOW 2 LIME SLURRY FEED 2 BLEED ** SOLIDS CONCENTRATING/DEWATERING THICKENER DEVICE NUMBER 1 α NUMBER OF SPARES CONFIGURATION CIRCULAR 85.0 DIA X 14.0 DIMENSIONS - FT SHELL GENERIC MATERIAL TYPE CARBON STEEL NONE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE N/A FEED STREAM SOURCE ABSORBER BLEED FEED STREAM CHARACTERISTICS 10% SOLIDS OUTLET STREAM CHARACTERISTICS 245 GPM, 25% SOLIDS OVERFLOW STREAM CHARACTERISTICS 185 GPM VACUUM FILTER CUTLET STREAM DISPOSITION OVERFLOW STREAM DISPOSITION LIME HOLD TANK & REACTION TANKS ** SOLIDS CONCENTRATING/DEWATERING VACUUM FILTER DEVICE NUMBER 2 NUMBER OF SPARES 1 CONFIGURATION CIRCULAR CAPACITY 500 GPM SHELL GENERIC MATERIAL TYPE NP SHELL SPECIFIC MATERIAL TYPE NR LINER GENERIC MATERIAL TYPE NR LINER SPECIFIC MATERIAL TYPE NR BELT GENERIC MATERIAL TYPE N/A BELT SPECIFIC MATERIAL TYPE N/A FEED STREAM SOURCE THICKENER UNDERFLOW FEED STREAM CHARACTERISTICS 25% SOLIDS OUTLET STREAM CHARACTERISTICS 60% SOLIDS *** SIUDGE FULL LOAD SLUDGE QUANTITY - M.TONS/HR (DRY) 5.7 (6.3 TPH) ** TREATMENT METHOD FIXATION DEVICE PUG MILL PROPRIETARY PROCESS CONVERSION SYSTEMS [POZ-O-TEC] INLET QUALITY - % 60.0 ** DISPOSAL NATURE FINAL TYPE LANDFILL LOCATION ON-SITE SITE TRANSPORTATION METHOD TRUCK SITE TREATMENT CLAY LINING SITE SERVICE LIFE - YRS 10 ** PROCESS CONTROL AND INSTRUMENTATION PROCESS STREAM RECYCLE LIQUOR CHEMICAL PARAMETERS PH CONTROL LEVELS PH 6.1-6.2 AT OUTLET & 8.5 AT INLET TO ABSORBER MONITOR LOCATION REACTION TANK PROCESS CONTROL MANNER AUTOMATIC

FEEDBACK

LOUISVILLE GAS & ELECTRIC: CANE RUN 4 (CONT.)

** WATER BALANCE

WATER LOOP TYPE OPEN/CLOSED RECEIVING WATER STREAM OHIO RIVER

MAKEUP WATER ADDITION - LITERS/S 6.3 (100 GPM)

** CHEMICALS AND CONSUMPTION

FUNCTION ABSORBENT

NAME BETZ POLYFLOC 1100

PRINCIPAL CONSTITUENT CA0H2
SOURCE/SUPPLIER AIRCO

CONSUMPTION 15000 LB/HR DRY CA(OH)2 AT FULL LOAD

UTILIZATION - % 100.0

POINT OF ADDITION RECYCLE TANK

** FGD SPARE CAPACITY INDICES

ABSORBER - % .0 MIST ELIMINATOR - % .0 REHEATER - % . 0 FAN - % .0 EFFLUENT HOLD TANK - % . 0 RECIRCULATION PUMP - % . 0 THICKENER - % . 0 VACUUM FILTER - % .0

** FGD SPARE COMPONENT INDICES

ABSORBER . 0 MIST ELIMINATOR . 0 REHEATER . 0 FAN .0 BALL MILL . 0 EFFLUENT HOLD TANK .0 RECIRCULATION PUMP . 0 THICKENER . 0 VACUUM FILTER .0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS HOURS FACTOR

8/76 SYSTEM 92.3 90.0 91.0 89.5 87.00 99.00 744 740 666 65.0

** PROBLEMS/SOLUTIONS/COMMENTS

INITIAL OPERATIONS OF THE CANE RUN 4 FGD SYSTEM BEGAN IN AUGUST WITH THE SYSTEM OPERATING 90% OF THE 740 HOURS THE BOILER WAS ON LINE.

OUTAGE TIME DURING THE MONTH WAS DUE PRIMARILY TO EQUIPMENT INSPECTIONS, REPAIR/REPLACEMENT OF AUXILIARY MOTOR PARTS, AND DEPLETION OF ABSORBENT SUPPLY BECAUSE OF A LATE BARGE DELIVERY.

THE SCRUBBING SYSTEM HAS BEEN GENERALLY OPERATING AT APPROXIMATELY 50 TO 80% FLUE GAS CAPACITY.

SOME MINOR PROBLEMS HAVE BEEN ENCOUNTERED WITH AUXILIARY EQUIPMENT MOTORS.

SOME MINOR PROBLEMS HAVE BEEN ENCOUNTERED WITH SPRAY NOZZLES IN THE MOBILE BED CONTACTOR. THE SPRAY NOZZLES ARE SPINNER-VANE COMPONENTS ORIGINALLY CONSTRUCTED OF PLASTIC. OPERATING TEMPERATURES AND PRESSURES HAVE CAUSED THE PLASTIC HOUSING TO EXPAND RESULTING IN THE VANES EXTRUDING OUT THE FRONT END, SUBSEQUENTLY CAUSING A BLOCKAGE OF THE SLURRY FEED. THE NOZZLES HAVE BEEN REPLACED WITH CERAMIC CONSTRUCTED COMPONENTS.

9/76 SYSTEM 91.5 90.0 90.5 90.0 88.00 720 720 648 62.0 10/76 SYSTEM 90.0 90.7 72.6 90.00 744 600 540 51.0 92.6

LOUISVILLE GAS & ELECTRIC: CANE RUN 4 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS TAKEN OUT OF SERVICE ON OCTOBER 25, 1976 TO IMPLEMENT ADDITIONAL MODIFICATIONS TO THE SCRUBBING SYSTEM. MAJOR SYSTEM MODIFICATIONS INCLUDE INCREASING PUMP CAPACITY AND DECREASING PRESSURE DROP. THESE TWO PROBLEMS HAVE HINDERED OPERATION OF THE UNIT AT FULL LOAD CAPACITY.

11/76	SYSTEM	96.0	95.0	94.0	79.2	89.00	720	600	570	52.0
12/76	SYSTEM	92.0	90.0	93.0	72.3	85.00	744	598	538	53.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT OPERATED ON CARBIDE LIME DURING THE NOVEMBER-DECEMBER PERIOD.

1/77 SYSTEM 42.0 37.7 40.0 33.7 86.00 744 666 251 32.0

** PROBLEMS/SOLUTIONS/COMMENTS

DUE TO OHIO RIVER FREEZE UP BARGE DELIVERIES OF LIME CEASED CAUSING THE FGD SYSTEM TO BE TAKEN OFF LINE ON JANUARY 12.

2/77 SYSTEM 100.0 1.2 672 0 8 .0

** PROBLEMS/SOLUTIONS/COMMENTS

DURING FEBRUARY, THE SCRUBBER WAS ONLY OPERATED FOR TWO 4-HOUR PERIODS TO PREVENT TOTAL FREEZE-UP.

3/77 SYSTEM 91.0 82.9 76.0 48.1 744 432 358 51.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE SCRUBBER CAME BACK ON-LINE ON MARCH 14, 1977.

DC POWER SUPPLY TO THE BYPASS DAMPER FAILED. THE SCRUBBER SYSTEM WAS BYPASSED WHILE REPAIRS WERE MADE.

4/77	SYSTEM	95.0	92.7	92.0	60.0	720	466	432	49.0
5/77	SYSTEM				.0	744		0	
6/77	SYSTEM				.0	720		0	

** PROBLEMS/SOLUTIONS/COMMENTS

THE SCRUBBING SYSTEM WAS DOWN FOR MODIFICATIONS FROM APRIL 19 TO JULY 17, 1977.

A CHEVRON TYPE MIST ELIMINATOR WAS INSTALLED DURING THE OUTAGE.

A NEW SPRAY HEADER WAS ADDED TO INCREASE THE L/G RATIO DURING THE OUTAGE.

DIRECT OIL-FIRED REHEAT WAS ADDED.

THE LINING IN THE SYSTEM FROM THE MIST ELIMINATOR TO THE STACK WAS RE-PLACED WITH PLASITE 4005 (THE ORIGINAL LINING WAS BUBBLING, BUT HAD NOT YET FAILED, FAILURE SEEMED IMMINENT WITHIN 4-5 MONTHS). THE NEW LINING WAS INSTALLED BY GENERAL COATINGS.

7/77 SYSTEM 95.0 90.0 90.0 43.5 744 360 324 36.0

PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% REMOVAL SO2 PART.	PER	BOILER	FGD	
	** PROE	SLEMS/SOLUTIO	NS/COMMENTS							
			THE SYSTEM WA			ON JULY 17	1977	AFTER	SYSTEM	
8/77	SYSTEM	79. 0	89.5	90.0	79.0		744	657	588	60.0
9/77	SYSTEM	98.9	99.1	99.0	72.8		720	529	524	59.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS							
			COMPLIANCE TESPERSONNEL AND							
10/77	SYSTEM	98.1	97.8	99.0	89.0		744	677	662	51.0
11/77	SYSTEM	69.9	94.0	94.0	62.9		720	483	453	53.0
12/77	SYSTEM	85.0	85.0	100.0	81.7		744	715	608	48.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS							
				BER, "AIRCO", UP CAUSING LI						
1/78	SYSTEM	66.4	66.6	87.0	66.4		744	742	494	50.0
2/78	SYSTEM	100.0			.0		672	0	0	.0
3/78	SYSTEM	100.0	33.5	35.0	33.5		744	744	249	52.0
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
		,	THE UNIT WAS I AND A LACK OF THE UNIT CAME	AVAILABLE LI	ME RESULTING	FROM THE SI		_		
4/78	SYSTEM	100.0	100.0	100.0	42.1		720	303	303	51.0
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
			THE BOILER W	AS DOWN PART	OF APRIL FOR	REPAIRS.				
5/78	SYSTEM	31.0	32.7	35.0	15.5		744	352	115	42.0
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
			THE BOILER W	AS DOWN AGAIN	DURING PART	OF MAY FOR	REPAI	RS.		
				AY BOILER OUT HE FGD SYSTEM		OF MODIFIC	ATIONS	WERE M	ADE TO	THE
6/78	SYSTEM	99.3	99.3	99.3	99.3		720	720	715	50.0
7/78	SYSTEM	98.8	98.7	98.7	91.1		744	687	678	44.0
8/78	SYSTEM	100.0	94.2	96.0	94.2		744	744	701	53.0
		100.0	100.0						138	

LOUISVILLE GAS & ELECTRIC: CANE RUN 4 (CONT.)

				PERFORMAN	NCE DATA						
			Y OPERABILITY R			% RE	MOVAL	PER	BOILER HOURS		CAP. FACTOR
	** 00081	FMS/SOLUT	CONS/COMMENTS								
	** PRODE		THERE WERE NO	FGD FODCED	OUTAGES DUD'T	NG TH	F AUGU	ST-SEPI	TEMBER	PERTON	
			THE BOILER WEN								•
			TUBE REPAIRS.	II DOMN IN	SEPTEMBER AFT	EK 13	o nook	3 Or Or	-LRAI IO	1 TOR	
10/78	SYSTEM	100.0	,		. 0			744	0	0	.0
	** PROBL	.EMS/SOLUT	ONS/COMMENTS								
			THE BOILER REM	AINED OFF	LINE DURING O	CTOBE	R FOR	CONTINU	MOITAL	OF THE	TUBE
11/78	SYSTEM	100.0	97.2	98.0	58.3			720	432	420	36.0
	** PROBL	EMS/SOLUT	ONS/COMMENTS								
			THE BOILER AND NOVEMBER WITH								F
12/78	SYSTEM	100.0			. 0			744	0	0	.0
	** PROBL	.EMS/SOLUT:	IONS/COMMENTS								
			DURING DECEMBE TO BE OFF LINE			ERATI	ONAL.	THE U	VIT IS	EXPECTE	ED
1/79	SYSTEM	100.0			.0			744	0	0	.0
2/79	SYSTEM	100.0			.0			672	0	0	.0
3/79	SYSTEM	100.0			.0			744	0	0	.0
4/79	SYSTEM	100.0			.0			720	0	0	.0
	** PROBL	.EMS/SOLUT	IONS/COMMENTS								
			THE UNIT DID NO					USE THE	BOILE	R WAS S	STILL
5/79	SYSTEM	100.0			.0			744	0	0	.0
6/79	SYSTEM	100.0	46.2	46.2	17.1			720	266	123	34.0
	** PROBL	.EMS/SOLUT	IONS/COMMENTS								
			THE UNIT REMAIN REPAIRS. THE U						AND BO	ILER Τ	JBE
7/79	SYSTEM	98.0	98.7	97.0	93.0			744	701	692	62.0
8/79	SYSTEM	92.0	89.2	89.0	89.2			744	744	664	61.0
9/79	SYSTEM		. 0		. 0			720	168	0	36.0
	** FROB	EMS/SOLUT	IONS/COMMENTS								
			THE ONLY MAJOR ENCOUNTERED CAU DAMPER GATES CA	JSING THE B	OILER OUTAGE	M DHA	ECHANI	CAL FA	ILURE W	ITH TH	
10/79	SYSTEM	72.0	30.1	70.0	12.0			744	296	89	39.0

•	MODULE AV	'AILABILITY	OPERABILITY	PERFORMANC RELIABILITY U	TILIZATION	% REMO \$02	OVAL PART. H	PER 10URS	BOILER HOURS	HOURS	
1/79	SYSTEM	96.0	93.9	94.0	58.1			720	445	418	42.0
2/79	SYSTEM	91.0	38.5	38.0	20.2			744	390	150	40.0
	** PROBLE	MS/SOLUTIO	NS/COMMENTS								
				JRTH QUARTER 1 5 WERE A RESUL					EMS.	THE LO	1
1/80	SYSTEM	100.0	100.0	99.0	95.6			744	711	711	53.0
2/80	SYSTEM	100.0	99.8	99.0	66.7			696	465	464	41.0
3/80	SYSTEM	82.0	80.5	80.0	74.3			744	687	553	55.0
	** PROBLE	MS/SOLUTIO	NS/COMMENTS								
				ATIONAL PROBLE HE BOILER OR T			FOR THI	E FIRS	ST QUAR	TER OF	1980
4/80	SYSTEM	99.0	98.8	98.8	79.9			720	582	575	48.0
	** PROBLE	EMS/SOLUTIO	NS/COMMENTS								
		c	OURING APRIL :	SPRAY PUMP PRO	BLEMS CAUSE	D SEVE	N HOURS	5 OF 0	OUTAGE '	TIME.	
5/80	SYSTEM	96.8	100.0	100.0	7.0			744	52	52	10.0
	** PROBLE	MS/SOLUTIO	NS/COMMENTS								
				S NOT NEEDED M		THIS .	ACCOUN	TS FOF	THE LO	DM	
		-	DNE DAY OF OU SEAL.	TAGE TIME IN P	MAS CAUS	SED BY	A LEAK	IN A	SPRAY I	PUMP	
6/80	SYSTEM	.0	.0		.0			720	350	0	32.0
	** PROBLE	EMS/SOLUTIO	NS/COMMENTS								
		-		F JUNE THE BOI LININGS WERE R		RESERV	E, IN I	WHICH	TIME T	HE SCRI	JBBER
				MADE TO MODULE WERE MADE WITH		אס סעכדו	WORK.	DUCTI	WORK RE	PAIRS/	
				HE DOWN TIME 1 R PUMP WAS REF		NIOL NO	T LOCA	TED A	T THE D	ISCHAR	GE
			92.8	92.8	85.7						
7/80		85.7									
7/80	A B System	85.7 85.7 85.7	92.8 92.8	92.8 92.8	85.7 85.7			744	687	638	58.0
7/80	B SYSTEM	85.7 85.7	92.8					744	687	638	58.0
7/80	B SYSTEM	85.7 85.7 EMS/SOLUTIO	92.8 92.8 DNS/COMMENTS		85.7	L REHEA	T SYST				58.0
7/80	B SYSTEM	85.7 85.7 EMS/SOLUTIO	92.8 92.8 DNS/COMMENTS PROBLEMS WERE	92.8	85.7 WITH THE OIL			בא סט	UL ƏMIЯ	LY.	
	B SYSTEM	85.7 85.7 EMS/SOLUTIO	92.8 92.8 DNS/COMMENTS PROBLEMS WERE	92.8 ENCOUNTERED O VALVE FAILUE	85.7 WITH THE OIL			בא סט	RING JU	LY. OUNTED	

LOUISVILLE GAS & ELECTRIC: CANE RUN 4 (CONT.)

6/81 SYSTEM

84.2

80.4

-----PERFORMANCE DATA-----PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS FACTOR ** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR OUTAGES OCCURRED DURING AUGUST AND SEPTEMBER. 744 10/80 SYSTEM 100.0 100.0 100.0 82.1 611 611 50.0 ** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE MONTH OF OCTOBER. 71.8 52.8 35.2 720 572 254 50.0 11/80 SYSTEM 52.8 ** PROBLEMS/SOLUTIONS/COMMENTS DURING NOVEMBER DUCTWORK FAILURE CAUSED SOME OUTAGE TIME. ALSO DURING THE MONTH PROBLEMS WERE ENCOUNTERED WHEN THE MIST ELIMINATORS FAILED. 76.8 12/80 SYSTEM 100.0 100.0 100.0 744 572 572 50.0 ** PROBLEMS/SOLUTIONS/COMMENTS DURING DECEMBER THE UTILITY REPORTED THAT NO FGD-RELATED PROBLEMS OCCURRED. 1/81 SYSTEM 81.0 81.0 81.0 81.0 744 744 604 35.0 ** PROBLEMS/SOLUTIONS/COMMENTS DURING JANUARY THE FGD SYSTEM WAS OUT OF SERVICE APPROXIMATELY 140 HOURS DUE TO A LACK OF AVAILABLE LIME. 2/81 SYSTEM . 0 . 0 .0 . 0 672 268 0 35.0 ** PROBLEMS/SOLUTIONS/COMMENTS DURING FEBRUARY THE FGD SYSTEM WAS NOT AVAILABLE DUE TO MIST ELIMINATOR AND DUCTWORK PROBLEMS. 3/81 SYSTEM 100.0 100.0 100.0 39.0 744 290 290 35.0 ** PROBLEMS/SOLUTIONS/COMMENTS DURING MARCH THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED. 4/81 SYSTEM 100.0 . 0 720 ٥ .0 5/81 SYSTEM 100.0 . 0 744 .0 ** PROBLEMS/SOLUTIONS/COMMENTS DURING THE MONTHS OF APRIL AND MAY THE UNIT DID NOT OPERATE. HOWEVER, THE FGD SYSTEM WAS AVAILABLE 100%.

80.4

63.6

720

570

458 50.0

PERIOD	MODULE AV	/AILABILI	TY OPERABILI	TY RELIABILITY	UTILIZATION				BOILER HOURS		
	** PROBLE	MS/SOLUT	IONS/COMMENT	S							
			DURING THE	MONTH OF JUNE	THE PUMP PIT	T WAS SI	JBMERGI	ED IN :	SLURRY.		
7/81	SYSTEM	72.6	100.0	100.0	72.6			744	540	540	50.0
8/81	SYSTEM	39.9	65.9	65.9	39.9			744	451	297	50.0
9/81	SYSTEM	60.8	100.0	100.0	60.8			720	438	438	50.0
	** PROBLE	MS/SOLUT	IONS/COMMENT	s							
				DULE PLUGGING DURING THE THE			MAJORI	TY OF	THE FGD	SYSTER	1
10/81	SYSTEM	65.4	93.3	93.3	65.4			744	522	487	40.0
11/81	SYSTEM	99.3	99.6	99.6	99.3			720	718	715	40.0
12/81	SYSTEM	65.4	100.0	100.0	65.4			744	487	487	40.0
	** PROBLE	EMS/SOLUT	IONS/COMMENT	'S							
			· · · · · · · · · · · · · · · · · · ·	REPORTED THAT		GD-RELA	TED PR	OBLEMS	WERE E	NCOUNTE	ERED
1/82	SYSTEM	11.0	4.0	4 0	3.0			744	557	22	54.0
	** PROBLE	EMS/SOLUT	IONS/COMMENT	·s							
				JARY, LOW SYSTE EZING THE MOB							TOR.
2/82	SYSTEM	.0	.0	.0	.0			672	0	0	50.0
3/82	SYSTEM	100.0	100.0	100.0	52.8			744	393	393	46.0
	** PROBLE	EMS/SOLUT	IONS/COMMENT	·s							
			FROM JANUAR REPAIRS.	Y 24 TO MARCH	8 THE UNIT	AND MOD	ULES W	ERE DO	WN FOR	GENERA	L
4/82	SYSTEM	97.1	96.4	96.4	70.6			720	527	506	50.0
5/82	SYSTEM	92.3	91.2	91.2	79.2			744	649	592	50.0
6/82	SYSTEM	94.6	93.8	93.8	81.7			720	627	588	50.0
	** PROBLI	EMS/SOLUT	'IONS/COMMEN	rs							
				REPORTED THAT SECOND QUARTER		GD-RELA	TED PR	OBLEMS	WERE E	NCOUNT	ERED
7/82	SYSTEM	74.7	81.5	81.5	74.7			744	682	556	50.0
8/82	SYSTEM	57.4	83.6	83.6	57.4			744	511	427	50.0
	SYSTEM	71.0	94.6	94.6	71.0			720	540	E11	50.0

LOUISVILLE GAS & ELECTRIC: CANE RUN 4 (CONT.)

			PERFORMAN	NCE DATA						
PERIOD MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% REI	MOVAL	PER	BOILER	FGD	CAP.
, =,,=======								HOURS		
		****		*****						

** PROBLEMS/SOLUTIONS/COMMENTS

REPAIRS ON THE ABSORBER MOBILE BED CONTACTORS RESULTED IN OUTAGE TIME DURING THE PERIOD OF JULY, AUGUST AND SEPTEMBER, 1982.

DUCTWORK REPAIRS ALSO ACCOUNTED FOR OUTAGE TIME DURING THE MONTHS OF JULY, AUGUST AND SEPTEMBER 1982.

10/82	SYSTEM	61.6	98.7	98.7	61.6	744	464	458	50.0
11/82	SYSTEM	75.6	99.8	99.8	75.6	720	545	544	50.0
12/82	SYSTEM	84.9	100.0	100.0	84.9	744	632	632	50.0
1/83	SYSTEM	72.3	99.1	99.1	72.3	744	543	538	50.0
2/83	SYSTEM	48.1	99.4	99.4	48.1	672	325	323	50.0
3/83	SYSTEM	57.5	95.5	95.5	57.5	744	448	428	50.0
4/83	SYSTEM	19.7	100.0	100.0	19.7	720	142	142	50.0
5/83	SYSTEM	16.1	97.6	97.6	16.1	744	123	120	50.0
6/83	SYSTEM	74.0	100.0	100.0	74.0	720	533	533	50.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE PERIOD OF APRIL THROUGH JUNE 1983.

7/83	SYSTEM	100.0			.0	744	0	0
8/83	SYSTEM	100.0			.0	744	0	0
9/83	SYSTEM	100.0	91.7	91.7	3.1	72 0	24	22

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE THIRD QUARTER OF 1983.

10/83	SYSTEM	100.0	99.3	99.3	55.1	744	413	410
11/83	SYSTEM	100.0	99.4	99.4	50.1	720	363	361
12/83	SYSTEM	39.9	36.5	36.5	18.5	744	364	133

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE REPORTED FOR THE FOURTH QUARTER OF 1983.

1/84	SYSTEM	744
2/84	SYSTEM	696
3/84	SYSTEM	744
4/84	SYSTEM	720
5/84	SYSTEM	744
6/84	SYSTEM	720

			 DFDFNDMAN	JCE DATA				 	
		AVAILABILITY			% REN	10VAL	PER	FGD	CAP.
7/84	SYSTEM						744		
8/84	SYSTEM						744		
9/84	SYSTEM						720		

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE FIRST THREE QUARTERS OF 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

LOUISVILLE GAS & ELECTRIC COMPANY NAME CANE RUN PLANT NAME UNIT NUMBER LOUISVILLE CTTY KENTUCKY STATE REGULATORY CLASSIFICATION 50. (.116 LB/MMBTU) 516. (1.200 LB/MMBTU) ****** (****** LB/MMBTU) PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW 992 NET PLANT GENERATING CAPACITY - MW
GROSS UNIT GENERATING CAPACITY - MW
NET UNIT GENERATING CAPACITY W/FGD - MW
NET UNIT GENERATING CAPACITY WO/FGD - MW 200 192 195 EQUIVALENT SCRUBBED CAPACITY - MW 200 ** UNIT DATA - BOILER AND STACK RILEY STOKER BOILER SUPPLIER BOILER TYPE PULVERIZED COAL CYCLING
349.21 (740000 ACFM)
148.9 (300 F)
76. (250 FT)
CONCRETE DESIGN BOILER FLUE GAS FLOW - CU.M/S
BOILER FLUE GAS TEMPERATURE - C
STACK HEIGHT - M BOILER SERVICE LOAD STACK SHELL 5.8 (19.0 FT) STACK TOP DIAMETER - M ** FUEL DATA FUEL TYPE COAL BITUMINOUS FUEL GRADE AVERAGE HEAT CONTENT J/G 25586. (11000 BTU/LB) RANGE HEAT CONTENT - BTU/LB 10400-11900 AVERAGE ASH CONTENT - % 13.90 13.90 10.0-20.0 9.00 RANGE ASH CONTENT - % RANGE ASH CUNTENT - %
AVERAGE MOISTURE CONTENT - % RANGE MOISTURE CONTENT - % 8.0-10.8 AVERAGE SULFUR CONTENT - % 3.80 3.5-4.0 RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % .04 0.03-0.06 RANGE CHLORIDE CONTENT - % *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER n TYPE NONE ** ESP NUMBER 2 NUMBER OF SPARES Ω TYPE COLD SIDE RESEARCH-COTTRELL 174.6 (370000 ACFM) SUPPLIER INLET FLUE GAS CAPACITY - CU.M/S
INLET FLUE GAS TEMPERATURE - C 148.9 (300 F) .0 (0. IN-H2O) 99.0 PRESSURE DROP - KPA PARTICLE REMOVAL EFFICENCY - % ** PARTICLE SCRUBBER NUMBER GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL N/A LINER GENERIC MATERIAL N/A LINER SPECIFIC MATERIAL N/A GAS CONTACTING DEVICE TYPE N/A

*** FGD SYSTEM

INUISVILLE GAS & ELECTRIC: CANE RUN 5 (CONT.)

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** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                               THROWAWAY PRODUCT
   SO2 REMOVAL MODE
                                               WET SCRUBBING
   PROCESS TYPE
                                               LIME
   PROCESS ADDITIVES
                                               NONE
   SYSTEM SUPPLIER
                                               COMBUSTION ENGINEERING
   A-E FIRM
                                               FLUOR - PIONEER
   DEVELOPMENT LEVEL
                                               FULL SCALE
   NEW/RETROFIT
                                               RETROFIT
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.00
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                 85.00
   ENERGY CONSUMPTION - %
                                                 1.5
   CURRENT STATUS
   COMMERCIAL START-UP
                                                7/78
   INITIAL START-UP
                                               12/77
   CONTRACT AWARDED
                                                4/75
** DESIGN AND OPERATING PARAMETERS
   DESIGN COAL SULFER CONTENT - %
                                                  4.00
   DESIGN COAL HEAT CONTENT - J/G
                                               25586.0
                                                              ( 11000 BTU/LB)
   DESIGN COAL ASH CONTENT - %
                                                 15.00
   DESIGN MOISTURE CONTENT - %
                                                 12.00
   DESIGN CHLORIDE CONTENT - %
                                                   .07
   OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                               304.0
** QUENCHER/PRESATURATOR
   NUMBER
                                                0
** ABSORBER
   NUMBER
                                                2
   NUMBER OF SPARES
                                                0
   GENERIC TYPE
                                               SPRAY TOWER
   SPECIFIC TYPE
                                               OPEN COUNTERCURRENT SPRAY
   TRADE NAME/COMMON TYPE
                                               N/A
   SUPPLIER
                                               COMBUSTION ENGINEERING
   DIMENSIONS - FT
                                               32.0 X 22.5
   SHELL GENERIC MATERIAL
                                               CARBON STEEL
   SHELL SPECIFIC MATERIAL
                                               AISI 1110
   SHELL MATERIAL TRADE NAME/COMMON TYPE
                                               N/A
   LÍNER GENERIC MATERIAL
                                               STAINLESS STEEL
   LINER SPECIFIC MATERIAL
                                               AUSTEMITIC
                                               TYPE 316L
   LINER MATERIAL TRADE NAME/COMMON TYPE
   GAS CONTACTING DEVICE TYPE
                                               NONE
   NUMBER OF CONTACTING ZONES
                                               3
   LIQUID RECIRCULATION RATE - LITER/S
                                               1102.
                                                            (17500 GPM)
                                                             ( 67.0 GAL/1000 ACF)
                                                   9.0
   L/G RATIO - L/CU.M
                                                             ( 2.0 IN-H20)
   GAS-SIDE PRESSURE DROP - KPA
                                                   . 5
                                                             ( 12.0 FT/S)
                                                  3.7
   SUPERFICAL GAS VELOCITY - M/SEC
                                                123.17
                                                             ( 261000 ACFM)
   INLET GAS FLOW - CU. M/S
   INLET GAS TEMPERATURE - C
                                                 52.2
                                                              ( 126 F)
   SO2 REMOVAL EFFICIENCY - %
                                                  85.0
   PARTICLE REMOVAL EFFICENCY - %
                                                  76.0
** MIST ELIMINATOR
   PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                               PRIMARY COLLECTOR
   NUMBER PER SYSTEM
                                                2
   NUMBER OF SPARES PER SYSTEM
                                               0
   NUMBER PER MODULE
                                               1
   GENERIC TYPE
                                               IMPINGEMENT
   SPECIFIC TYPE
                                               BAFFLE
   TRADE NAME/COMMON TYPE
                                               CLOSED VANE
                                               HORIZONTAL
   CONFIGURATION
   NUMBER OF STAGES
                                                   2
   NUMBER OF PASSES PER STAGE
                                                   3
                                                              ( .5 IN-H20)
   PRESSURE DROP - KPA
                                                   .1
                                                   2.1
   SUPERFICAL GAS VELOCITY - M/S
                                                              ( 7.0 FT/S)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              ORGANIC
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               FIBER-REINFORCED POLYESTER
   WASH WATER SOURCE
                                               RIVER
                                               ONCE PER SHIFT
   WASH FREQUENCY
```

LOUISVILLE GAS & ELECTRIC: CANE RUN 5 (CONT.)

```
5.0
                                                              ( 80 GAL/MIN)
   WASH RATE - L/S
** REHEATER
                                                2
   NUMBER
   NUMBER OF SPARES
                                                0
   NUMBER PER MODULE
                                                1
    GENERIC TYPE
                                               IN-LINE
                                               STEAM
    SPECIFIC TYPE
    TRADE NAME/COMMON TYPE
                                               FIN TUBE
    COMBUSTION FUEL SULFER CONTENT - %
                                                    . ก
                                               10 FT BEYOND THE ABSORBER OUTLET
    LOCATION
    PERCENT GAS BYPASSED - AVG
                                                    ۰.0
    TEMPERATURE INCREASE - C
                                                  13.9
                                                                  25 F)
    INLET FLUE GAS FLOW RATE - CU. M/S
                                                 265.21
                                                              ( 562000 ACFM)
                                                             ( 130 F)
    INLET FLUE GAS TEMPERATURE - C
                                                 54.4
                                                              ( 155 F)
    OUTLET FLUE GAS TEMPERATURE - C
                                                 68.3
    NUMBER OF TUBES PER BUNDLE
                                                 34
    CONSTRUCTION MATERIAL GENERIC TYPE
                                              CARBON STEEL
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              AISI 1110
** FANS
   NUMBER
                                                2
    NUMBER OF SPARES
                                                0
    DESIGN
                                               CENTRIFUGAL
    FUNCTION
                                               UNIT
    APPLICATION
                                               FORCED DRAFT
    SERVICE
                                               DRY
    FLUE GAS FLOW RATE - CU.M/S
                                                              ( 350000 ACFM)
                                                165.16
    FLUE GAS TEMPERATURE - C
                                                 148.9
                                                              ( 300 F)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL
** FANS
   NUMBER
                                                2
    NUMBER OF SPARES
                                                n
    DESIGN
                                               CENTRIFUGAL
    FUNCTION
                                               BOOSTER
    APPLICATION
                                               INDUCED DRAFT
    SERVICE
                                               DRY
    FLUE GAS TEMPERATURE - C
                                                  68.3
                                                              ( 155 F)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL
** DAMPERS
    NUMBER
                                                2
    FUNCTION
                                               SHUT-OFF
    GENERIC TYPE
                                               LOUVER
    MANUFACTURER
                                               COMBUSTION ENGINEERING
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL/STAINLESS STEEL [BLADES]
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               AISI 1110; AUSTENITIC
    LINER GENERIC MATERIAL TYPE
                                               NONE
    LINER SPECIFIC MATERIAL TYPE
                                               N/A
** DAMPERS
   NUMBER
                                                2
    FUNCTION
                                               SHUT-OFF
    GENERIC TYPE
                                               LOUVER
   MANUFACTURER
                                               COMBUSTION ENGINEERING
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL/STAINLESS STEEL [BLADES]
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               AISI 1110; AUSTENITIC
    LINER GENERIC MATERIAL TYPE
                                               NONE
    LINER SPECIFIC MATERIAL TYPE
                                               N/A
** DAMPERS
   NUMBER
                                                2
   FUNCTION
                                               SHUT-OFF
    GENERIC TYPE
                                               LOUVER
   MANUFACTURER
                                               COMBUSTION ENGINEERING
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL/STAINLESS STEEL [BLADES]
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               AISI 1110; AUSTENITIC
   LINER GENERIC MATERIAL TYPE
                                               NONE
    LINER SPECIFIC MATERIAL TYPE
                                               N/A
```

INITSVILLE GAS & ELECTRIC: CANE RUN 5 (CONT.)

```
** DUCTWORK
   LOCATION
                                               INLET TO ABSORBER & OUTLET FROM REHEATER
    SHELL GENERIC MATERIAL TYPE
                                               CARBON STEEL
    SHELL SPECIFIC MATERIAL TYPE
                                               AISI 1110
    LINER GENERIC MATERIAL TYPE
                                               NONE
    LINER SPECIFIC MATERIAL TYPE
                                               N/A
** DUCTWORK
   LOCATION
                                               OUTLET FROM ABSORBER TO REHEATER
    SHELL GENERIC MATERIAL TYPE
                                              CARBON STEEL
    SHELL SPECIFIC MATERIAL TYPE
                                               AISI 1110
    LINER GENERIC MATERIAL TYPE
                                               ORGANIC
    LINER SPECIFIC MATERIAL TYPE
                                               MICA FLAKE-FILLED POLYESTER
** REAGENT PREPARATION EQUIPMENT
   FUNCTION
                                               WET BALL MILL
   DEVICE TYPE
                                               TUBE MILL
   NUMBER
                                                1
   NUMBER OF SPARES
                                                0
   PRODUCT QUALITY - % SOLIDS
                                                  25.0
** TANKS
   SEPVICE
                                               NUMBER
                                               ____
   ABSORBER RECYCLE
                                                  2
   REAGENT PREP PRODUCT
                                                  1
** PUMPS
                                               NUMBER
   SERVICE
                                               -----
   ABSORBER RECIRCULATION
   LIME FEED
                                                  2
   THICKENER UNDERFLOW
                                                  2
   WATER RECYCLE
                                                  2
   MIST ELIMINATOR WASH
                                               ****
** SOLIDS CONCENTRATING/DEWATERING
                                               THICKENER
   DEVICE
   NUMBER
                                                1
   NUMBER OF SPARES
   CONFIGURATION
                                               CIRCULAR
   DIMENSIONS - FT
                                               110.0 DIA
                                               CARBON STEEL
   SHELL GENERIC MATERIAL TYPE
   SHELL SPECIFIC MATERIAL TYPE
                                               AISI 1110
                                              NONE
   LINER GENERIC MATERIAL TYPE
   LINER SPECIFIC MATERIAL TYPE
                                              N/A
                                               ABSORBER BLEED
   FEED STREAM SOURCE
                                              7% SOLIDS
   FEED STREAM CHARACTERISTICS
                                              250 GPM, 25% SOLIDS
   OUTLET STREAM CHARACTERISTICS
                                              250 GPM
   OVERFLOW STREAM CHARACTERISTICS
                                               VACUUM FILTER
   OUTLET STREAM DISPOSITION
                                               RECYCLE TANK AND THEN REACTION TANK
   OVERFLOW STREAM DISPOSITION
** SOLIDS CONCENTRATING/DEWATERING
                                               VACUUM FILTER
   DEVICE
                                               2
   NUMBER
   NUMBER OF SPARES
                                               CIRCULAR
   CONFIGURATION
   SHELL GENERIC MATERIAL TYPE
                                               NR
                                               NR
   SHELL SPECIFIC MATERIAL TYPE
   LINER GENERIC MATERIAL TYPE
                                               ИR
                                               NR
   LINER SPECIFIC MATERIAL TYPE
   BELT GENERIC MATERIAL TYPE
                                               NR
   BELT SPECIFIC MATERIAL TYPE
                                               ΝR
                                               THICKENER UNDERFLOW
   FEED STREAM SOURCE
                                               25% SOLIDS
   FEED STREAM CHARACTERISTICS
```

*** SLUDGE

LOUISVILLE GAS & ELECTRIC: CANE RUN 5 (CONT.)

FULL LOAD SLUDGE QUANTITY - M.TONS/HR (DRY) 14.3 (15.7 TPH)

** TREATMENT

FIXATION METHOD PUG MILL DEVICE

PROPRIETARY PROCESS CONVERSION SYSTEMS [POZ-Q-TEC]

** DISPOSAL

FINAL NATURE LANDFILL TYPE ON-SITE LOCATION SITE TRANSPORTATION METHOD TRUCK CLAY LINING SITE TREATMENT

SITE SERVICE LIFE - YRS

** PROCESS CONTROL AND INSTRUMENTATION

PROCESS STREAM CHEMICAL PARAMETERS PH PH 9 AT OUTLET & PH 5.4-5.6 AT INLET TO RECYCLE CONTROL LEVELS REACTION TANK MONITOR LOCATION AUTOMATIC PROCESS CONTROL MANNER FEEDBACK PROCESS CHEMISTRY MODE

10

ABSORBER RECYCLE LINE

** WATER BALANCE

WATER LOOP TYPE OPEN/CLOSED OHIO RIVER RECEIVING HATER STREAM

** CHEMICALS AND CONSUMPTION

ABSORBENT FUNCTION CARBIDE LIME NAME CAOH2 PRINCIPAL CONSTITUENT SOURCE/SUPPLIER AIRCO CONSUMPTION 137,000 TPY UTILIZATION - X 95.0

POINT OF ADDITION SLURRY FEED TANK

** FGD SPARE CAPACITY INDICES

.0 ABSCRBER % MIST ELIMINATOR - % .0 .0 REHEATER - % FAN % .0 BALL MILL - % .0 EFFLUENT HOLD TANK % .0 RECIRCULATION PUMP - 2 . 0 THICKENER % .0 VACUUM FILTER - % .0

** FGD SPARE COMPONENT INDICES

ABSORBER .0 MIST ELIMINATOR .0 REHEATER . 0 .0 BALL MILL .0 EFFLUENT HOLD TANK . 0 RECIRCULATION PUMP .0 THICKENER .0 VACUUM FILTER .0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS HOURS FACTOR

12/77 SYSTEM 744 LOUISVILLE GAS & ELECTRIC: CANE RUN 5 (CONT.)

		PERFORMAN	NCE DATA						
PERIOD MODULE AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% REI	MOVAL	PER	BOILER	FGD	CAP.
				S 02	PART.	HOURS	HOURS	HOURS	FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

OPERATION OF THE FGD SYSTEM, ON A TRIAL BASIS, BEGAN ON DECEMBER 29, 1977. INITIAL OPERATIONS WERE NOT CONTINUOUS AND THE SYSTEM WAS TAKEN OFF LINE FOR NECESSARY MODIFICATIONS.

1/78 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

MODIFICATIONS, ESPECIALLY TO CONTROLS THAT WERE NOT OPERATING PROPERLY, CONTINUED THROUGH JANUARY AND THE FGD SYSTEM REMAINED OFF LINE.

2/78	SYSTEM					672			
3/78	SYSTEM	60.0	50.0	50.0	12.2	744	182	91	27.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE PLANT REMAINED OFF LINE THROUGHOUT FEBRUARY AND RESTARTED ON MARCH 24.

VARIOUS INITIAL START-UP PROBLEMS WERE STILL BEING ENCOUNTERED CAUSING FGD SYSTEM OUTAGES.

4/78	SYSTEM	100.0	96.9	96.0	90.0	720	669	648	52.0
5/78	SYSTEM	91.0	84.3	84.0	48.9	744	432	364	36.0

** PROBLEMS/SOLUTIONS/COMMENTS

FGD SYSTEM MODIFICATIONS WERE MADE DURING THE APRIL-MAY PERIOD IN PREPARATION FOR PERFORMANCE TESTS. THE TESTS WERE PERFORMED; HOWEVER, THE TEST METHODS WERE NOT FOLLOWED ACCURATELY AND THE DATA WAS INCONCLUSIVE.

6/78	SYSTEM	86.8	86.1	36.0	81.9	720	685	590	51.0
7/78	SYSTEM	83.1	80.1	80.0	68.0	744	632	506	48.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE STEAM REHEAT COIL INSTALLATION HAS BEEN A CHRONIC PROBLEM AREA. WELDS HAVE BEEN FAILING EVER SINCE INITIAL OPERATIONS.

8/78	SYSTEM	76.0	85.9	85.0	62.4	744	540	464	42.0
9/78	SYSTEM	96.0	79.6	79.0	67.4	720	609	485	44.0

** PROBLEMS/SOLUTIONS/COMMENTS

PROBLEMS CONTINUED WITH THE REHEAT COILS.

10/78	SYSTEM	96.0	96.2	95.0	68.5	744	530	510	41.0
11/78	SYSTEM	95.0	93.7	94.0	32.9	720	253	237	40.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE SYSTEM WAS SHUTDOWN IN NOVEMBER FOR REPAIRS TO THE STEAM REHEATER COILS. THE OUTAGE LASTED ABOUT TWO WEEKS.

12/78	SYSTEM	52.7	46.2	46.0	40.6	744	654	302	47.0
1/79	SYSTEM	69.6	67.2	67.0	62.8	744	693	467	42.0

LOUISVILLE GAS & ELECTRIC: CANE RUN 5 (CONT.)

			OPERABILITY R								CAP.
PERIOD									HOURS		
2/79	SYSTEM	77.0	70.6	70. 0	50.1			672	477	337	42.0
27.			NS/COMMENTS								
		ם	URING FEBRUARY	FREEZING C	AUSED PROBLE	MS WI	TH LIM	E DELIV	/ERY.		
3/79	SYSTEM	77.0	71.8	71.0	57.5			744	596	428	41.0
4/79	SYSTEM	99.0	99.2	99.0	49.6			720	360	357	45.0
	** PROBL	_EMS/SOLUTIO	NS/COMMENTS								
		5	OME PROBLEMS W	ERE EXPERIE	NCED WITH DA	MPERS	AND T	HERE WI	ERE PUMI	P FAILU	RES.
5/79	SYSTEM	89.0	84.3	84.0	49.1			744	433	365	38.0
	** PROBL	EMS/SOLUTIO	NS/COMMENTS								
			COMPLIANCE TES AND A SO2 REMO DECLARED COMME	VAL EFFICIE	NCY OF 93% W	AS DE	MONSTR	ATED.			
6/79	SYSTEM	81.0	77.0	77.0	58.2			720	544	419	40.0
	** PROBL	_EMS/SOLUTIO	NS/COMMENTS								
			THE ONLY PROBLE								RE
7/79	SYSTEM	78.0	72.0	72. 0	56 .5			744	583	420	38.0
8/79	SYSTEM	90.0	88.1	88.0	72.6			744	613	540	46.0
9/79	SYSTEM	90.0	83.6	82.0	54.4			720	469	392	45.0
	** PROBI	_EMS/SOLUTIO	NS/COMMENTS								
		9	THE WELDING PRO SEPTEMBER. THE BY THIS WINTER.	FAILURES A							/ED
10/79	SYSTEM	87.0	83.7	85.0	65.6			744	583	488	42.0
11/79	SYSTEM	97.0	95.2	95 .0	46.4			720	351	334	41.0
12/79	SYSTEM	86.0	82.2	82.0	63.4			744	574	472	44.0
	** PROBI	LEMS/SOLUTIO	ONS/COMMENTS								
			OURING THE FOUR PROBLEMS OCCURR							MAJOR	
1/80	SYSTEM	94.0	92.1	92.0	72.2			744	583	537	43.0
	** PROBI	LEMS/SOLUTIO	DNS/COMMENTS								
		C	DURING JANUARY	NO OPERATIO	NAL PROBLEMS	S WERE	ENCOU	NTERED	•		
2/80	SYSTEM	81.0	71.9	71.0	49.7			696	481	346	50.0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

IN FEBRUARY THE UTILITY RAN OUT OF CARBIDE LIME CAUSING INTERRUPTION OF THE FGD SYSTEM OPERATION. THE UNAVAILABILITY OF LIME WAS CAUSED BY FREEZE UPS ENCOUNTERED BY AIRCO, THE LIME SUPPLIER.

3/80 SYSTEM 66.0 44.5 44.0 27.2 744 454 202 29.0

** PROBLEMS/SOLUTIONS/COMMENTS

REHEATER TUBE PROBLEMS WERE ENCOUNTERED IN FEBRUARY AND CONTINUED THROUGH MARCH. THE UTILITY HOPES TO REPLACE THE TUBE BUNDLES IN THE SUMMER.

4/80 SYSTEM .0 .0 720 0 0 .0

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS OFF LINE THE ENTIRE MONTH OF APRIL TO INSTALL STAINLESS STEEL (316 SS) IN THE DUCTWORK AND IN THE MODULES.

5/80 SYSTEM 95.3 94.5 94.5 80.2 744 632 597 43.0

** PROBLEMS/SOLUTIONS/COMMENTS

DURING MAY ONE DAY OF OUTAGE TIME WAS NECESSARY TO COMPLETE THE INSTALLATION OF THE STAINLESS STEEL IN THE DUCTWORK AND MODULES.

A PUMP SEAL ON THE RECIRCULATION PUMP FAILED CAUSING APPROXIMATELY 10 HOURS OF OUTAGE TIME.

6/80 SYSTEM 78.8 74.4 **74.**4 61.8 720 598 445 46.0

** PROBLEMS/SOLUTIONS/COMMENTS

DURING JUNE THE SYSTEM HAD TO BE TAKEN OFF LINE FOR 153 HOURS DUE TO THE POOR WELDS ON THE TUBE BUNDLES IN THE REHEATER. THE TUBE BUNDLES HAVE BEEN A CONSTANT PROBLEM AND THE MANUFACTURER IS SCHEDULED TO REPLACE THEM IN THE FALL.

7/80 SYSTEM 78.7 87.6 87.6 78.7 744 669 586 50.0

** PROBLEMS/SOLUTIONS/COMMENTS

DURING JULY THE REHEAT TUBE EXCHANGERS FAILED. TWO NEW EXCHANGERS ARE NOW ON SITE AND ARE SCHEDULED TO BE INSTALLED IN NOVEMBER OR DECEMBER 1980.

A THREE DAY OUTAGE OCCURRED IN JULY DUE TO A LIMESTONE ROCK DISABLING THE THICKENER.

744 8/80 SYSTEM 58.4 49.6 632 369 50.0 58.4 49.6 9/80 SYSTEM 97.5 87.2 720 644 628 50.0 97.5 87.2

** PROBLEMS/SOLUTIONS/COMMENTS

THE OUTAGE TIME DURING AUGUST AND SEPTEMBER WAS CAUSED BY A REHEAT TUBE BUNDLE FAILURE. THE BUNDLES ARE PRESENTLY BEING REPLACED IN BOTH MODULES.

10/80	SYSTEM	100.0	100.0	100.0	10.0	744	72	72	50.0
11/80	SYSTEM	100.0	100.0	100.0	25.0	720	177	177	50.0
12/80	SYSTEM	100.0	100.0	100.0	99.8	744	743	742	50.0

LOUISVILLE GAS & ELECTRIC: CANE RUN 5 (CONT.)

PERIOD	MODULE	AVAILABILI	TY OPERABILITY	RELIABILITY		SO2 PART.				
	** FRO	3LEMS/SOLUT	IONS/COMMENTS							
			THE UTILITY F		NO FGD-RELAT	ED PROBLEMS	WERE 1	ENCOUNT	ERED DI	RING
1/81	SYSTEM	100.0	99.7	99.7	89.4		744	667	665	50.0
	** PRO	BLEMS/SOLUT	IONS/COMMENTS							
			DURING JANUAR ENCOUNTERED.	Y THE UTILIT	Y REPORTED TH	ROLAM ON TAI	FGD-RI	ELATED	PROBLE	15 WERE
2/81	SYSTEM	82.0	77.0	77.0	59.0		672	512	394	50.0
	** PRO	BLEMS/SOLUT	IONS/COMMENTS							
			DURING FEBRUA	ARY SOME OUTA	GE TIME WAS D	UE TO FAN PI	ROBLEM	s.		
			ADDITIONAL PR	ROBLEMS WERE	ENCOUNTERED D	DUE TO REHEA	TER LE	AKS.		
3/81	SYSTEM	100.0	46.0	46.0	43.0		744	698	319	50.0
	** PRO	BLEMS/SOLUT	IONS/COMMENTS							
			OUTAGE TIME	OURING MARCH	WAS DUE TO ST	RIKING WORK	ERS AT	THE PL	ANT.	
4/81	SYSTEM	100.0	100.0	100.0	51.0		720	367	367	40.0
5/81	SYSTEM	100.0	95.9	95.9	92.3		744	716	687	45.0
	** PRO	BLEMS/SOLUT	TIONS/COMMENTS							
			_	REPORTED THAT		-RELATED PR	OBLEMS	WERE E	NCOUNT	ERED
6/81	SYSTEM	100.0			.0		720	0	0	.0
	** PRO	BLEMS/SOLUT	TIONS/COMMENTS							
				ONTH OF JUNE VAILABLE 100%		ID NOT OPERA	TE; HO	WEVER,	THE FG	D
7/81	SYSTEM	45.6	100.0	100.0	45.6		744	339	3 39	50.0
8/81	SYSTEM	49.5	100.0	100.0	49.5		744	368	3 68	45.0
9/81	SYSTEM	75.0	100.0	100.0	75.0		720	540	540	45.0
	** PRO	BLEMS/SOLUT	IONS/COMMENTS							
			THERE WERE N	O MAJOR FGD R	ELATED PROBLE	EMS REPORTED	FOR T	HE THIR	D QUAR	TER
10/81	SYSTEM	93.4	100.0	100.0	57.7		744	429	429	40.0
73 (03	SYSTEM	88.9	99.5	99.5	57.4		720	415		40.0

744 738 734 40.0

12/81 SYSTEM 98.6 99.4 99.4 98.6

720 527 527 50.0

6/83 SYSTEM 73.2 100.0

ERIOD	MODULE	AVAILABILIT	Y OPERABILITY	RELIABILITY	UTILIZATION	% REM	OVAL	PER	BOILER HOURS		
	** PROE	SLEMS/SOLUTI	ONS/COMMENTS								
			THE UTILITY R			D-RELAT	ED PRO	OBLEMS	WERE E	NCOUNT	ERED
1/82	SYSTEM	100.0	70.4	70.4	59.1			744	625	440	39.0
2/82	SYSTEM	100.0	91.0	91.0	49.6			672	366	3 33	50.0
3/82	SYSTEM	100.0	83.3	83.3	57 .5			744	514	428	35.0
	** PRO	SLEMS/SOLUTI	ONS/COMMENTS								
			THE UTILITY R			D-RELAT	ED PRO	DBLEMS	WERE E	NCOUNT	ERED
4/82	SYSTEM	100.0	100.0	100.0	15.6			720	112	112	50.0
5/82	SYSTEM	100.0	100.0	100.0	80.4			744	598	598	50.0
6/82	SYSTEM	96.2	96.0	96.0	89.0			720	668	641	50.0
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS								
			THE UTILITY R			D-RELAT	ED PRO	OBLEMS	WERE E	чсоинті	ERED
7/82	SYSTEM	87.8	96.2	96.2	87.8			744	679	653	50.0
8/82	SYSTEM	86.3	100.0	100.0	86.3			744	642	642	50.0
9/82	SYSTEM	33.5	97.2	100.0	33.5			720	248	241	50.0
	** PRO	BLEMS/SOLUTI	CONS/COMMENTS								
			THE UTILITY R DURING THE PE						WERE E	ИСОИНТІ	ERED
10/82	SYSTEM	.0			.0			744	0	0	50.0
11/82	SYSTEM	.0			.0			720	0	0	50.0
12/82	SYSTEM	.0			.0			744	0	0	50.0
	** PRO	BLEMS/SOLUTI	CONS/COMMENTS								
			A UNIT OVERHA			THE PER	RIOD O	F OCTO	BER THR	OUGH D	ECEMBER
1/83	SYSTEM	61.3	100.0	100.0	61.3			744	456	456	50.0
2/83	SYSTEM	65.6	99.3	99.3	65.6			672	444	441	50.0
3/83	SYSTEM	59.5	98.7	98.7	59.5			744	449	443	50.0
4/83	SYSTEM	43.6	100.0	100.0	43.6			720	314	314	50.0
	SYSTEM	89.4	99.4	99.4	89.4			744	669	445	50.0

100.0

73.2

LOUISVILLE GAS & ELECTRIC: CAME RUN 5 (CONT.)

PERFORMANCE DATA					
PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION	% REMOVAL	PER	BOILER	FGD	CAP.
	SO2 PART.	HOURS	HOURS	HOURS	FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE PERIOD OF JANUARY THROUGH JUNE 1983.

7/8	S SYSTEM	69.1	100.0	100.0	69.1	744	514	514	50.0
8/8	SYSTEM	29.0	39.3	39.3	29.0	744	549	216	50.0
9/8	S SYSTEM	83.6	97.6	97 .6	55.4	720	409	399	50.0

** PROBLEMS/SOLUTIONS/COMMENTS

LOW AVAILABILITY DURING THE THIRD QUARTER WAS DUE IN PART TO GENERAL REPAIRS RESULTING FROM CORROSION PROBLEMS.

10/83	SYSTEM	10.9	100.0	100.0	2.0	744	15	15
11/83	SYSTEM	67.6	91.2	91.0	53.2	720	420	383
12/83	SYSTEM	44.0	45.1	45.1	25.5	744	421	190

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE REPORTED FOR THE FOURTH QUARTER OF 1983.

1/84	SYSTEM	744
2/84	SYSTEM	696
3/84	SYSTEM	744
4/84	SYSTEM	720
5/84	SYSTEM	744
6/84	SYSTEM	720
7/84	SYSTEM	744
8/84	SYSTEM	744
9/84	SYSTEM	720

^{**} PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE FIRST THREE QUARTERS OF 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

LOUISVILLE GAS & ELECTRIC COMPANY NAME PLANT NAME CANE RUN UNIT NUMBER LOUISVILLE CITY KENTUCKY STATE E 50. (.116 LB/MMBTU) 516. (1.200 LB/MMBTU) ****** (****** LB/MMBTU) REGULATORY CLASSIFICATION PARTICULATE EMISSION LIMITATION - NG/J SOZ EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J 99**2** 299 NET PLANT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW NET UNIT GENERATING CAPACITY W/FGD - MW 277 NET UNIT GENERATING CAPACITY WO/FGD - MW 280 EQUIVALENT SCRUBBED CAPACITY - MW 299 ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER COMBUSTION ENGINEERING PULVERIZED COAL BOILER TYPE BOILER SERVICE LOAD BASE DESIGN BOILER FLUE GAS FLOW - CU.M/S BOILER FLUE GAS TEMPERATURE - C 502.57 502.57 (1065000 ACFM) 148.9 (300 F) 158. (518 FT) STACK HEIGHT - M CONCRETE 4.9 (16.0 FT) STACK SHELL STACK TOP DIAMETER - M ** FUEL DATA FUEL TYPE COAL BITUMINOUS FUEL GRADE 25586. (11000 BTU/LB) AVERAGE HEAT CONTENT - J/G RANGE HEAT CONTENT - BTU/LB 10400-11900 17.06 AVERAGE ASH CONTENT - % 15.5-24.5 RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - % 8.95 RANGE MOISTURE CONTENT - % 8.0-10.8 AVERAGE SULFUR CONTENT - % 4.80 3.5-6.3 RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % .04 RANGE CHLORIDE CONTENT - % 0.03-0.06 *** PARTICLE CONTROL ** MECHANICAL COLLECTOR 0 NUMBER NONE TYPE ** FABRIC FILTER NUMBER 0 TYPE NONE ** ESP NUMBER 2 COLD SIDE TYPE 251.8 (533500 ACFM) 148.9 (300 F) INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE - C 99.4 PARTICLE REMOVAL EFFICENCY - % ** PARTICLE SCRUBBER NUMBER NONE GENERIC TYPE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A N/A SHELL GENERIC MATERIAL SHELL SPECIFIC MATERIAL N/A N/A LINER GENERIC MATERIAL N/A LINER SPECIFIC MATERIAL GAS CONTACTING DEVICE TYPE N/A

LOUISVILLE GAS & ELECTRIC: CANE RUN 6 (CONT.)

*** FGD SYSTEM

** GENERAL DATA SALEABLE PRODUCT/THROWAWAY PRODUCT SO2 REMOVAL MODE PROCESS TYPE SYSTEM SUPPLIER A-E FIRM DEVELOPMENT LEVEL NEW/RETROFIT UNIT DESIGN PARTICLE REMOVAL EFFICIENCY UNIT DESIGN SO2 REMOVAL EFFICIENCY - % ENERGY CONSUMPTION - % CURRENT STATUS COMMERCIAL START-UP INITIAL START-UP CONTRACT AWARDED	
** DESIGN AND OPERATING PARAMETERS	
** QUENCHER/PRESATURATOR CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE	NR NR
** ABSORBER	
** ABSORBER NUMBER GENERIC TYPE SPECIFIC TYPE TRADE NAME/COMMON TYPE SUPPLIER DIMENSIONS - FT SHELL GENERIC MATERIAL SHELL SPECIFIC MATERIAL SHELL MATERIAL TRADE NAME/COMMON TYPE LINER GENERIC MATERIAL LINER SPECIFIC MATERIAL LINER MATERIAL TRADE NAME/COMMON TYPE GAS CONTACTING DEVICE TYPE NUMBER OF CONTACTING ZONES LIQUID RECIRCULATION RATE - LITER/S L/G RATIO - L/CU.M GAS-SIDE PRESSURE DROP - KPA SUPERFICAL GAS VELOCITY - M/SEC INLET GAS TEMPERATURE - C SO2 REMOVAL EFFICIENCY - %	2 TRAY TOWER SIEVE TRAY N/A THYSSEN/CEA 32.0 DIA X 45.0 CARBON STEEL ASTM A-283 N/A ORGANIC MICA FLAKE-FILLED POLYESTER NR PERFORATED TRAYS 2 272. (4318 GPM)
** MIST ELIMINATOR PRE-MIST ELIMINATOR/MIST ELIMINATOR NUMBER PER SYSTEM GENERIC TYPE SPECIFIC TYPE TRADE NAME/COMMON TYPE CONFIGURATION NUMBER OF STAGES NUMBER OF PASSES PER STAGE FREEBOAPD DISTANCE - M PRESSURE DROP - KPA SUPERFICAL GAS VELOCITY M/S CONSTRUCTION MATERIAL SPECIFIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE	PRIMARY COLLECTOR 2 IMPINGEMENT BAFFLE CLOSED VANE HORIZONTAL 1 4 1.52 (5.0 FT) .2 (1.0 IN-H20) 2.7 (9.0 FT/S) ORGANIC POLYPROPYLENE
** REHEATER NUMBER GENEPIC TYPE SPECIFIC TYPE TPADE NAME/COMMON TYPE PERCENT GAS BYPASSED - AVG TEMPERATUPE INCREASE C INLET FLUE GAS FLOW RATE - CU. M/S	2 DIRECT COMBUSTION EXTERNAL COMBUSTION CHAMBER OIL .0 27.8 (50 F) 205.98 (436500 ACFM)

IOUISVILLE GAS & ELECTRIC: CANE RUN 6 (CONT.)

THLET FLUE GAS TEMPERATURE - C 51.7 (125 F) ND CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE NR ** FANS NUMBER DESTGN CENTRIFUGAL FUNCTION **BOOSTER** FORCED DRAFT **APPLICATION** SERVICE DRY FLUE GAS FLOW RATE - CU.M/S 251.52 (533000 ACFM) FLUE GAS TEMPERATURE - C 148.9 (300 F) CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL ** DAMPERS FUNCTION NR GENERIC TYPE NP SPECIFIC TYPE NR CONSTRUCTION MATERIAL GENERIC TYPE ND CONSTRUCTION MATERIAL SPECIFIC TYPE NR LINER GENERIC MATERIAL TYPE NR LINER SPECIFIC MATERIAL TYPE NR ** DUCTWORK SCRUBBER INLET LOCATION SHELL GENERIC MATERIAL TYPE CARBON STEEL SHELL SPECIFIC MATERIAL TYPE AISI 1110 LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DUCTWORK LOCATION SCRUBBER TO REHEATER SHELL GENERIC MATERIAL TYPE CARBON STEEL SHELL SPECIFIC MATERIAL TYPE AISI 1110 LINER GENERIC MATERIAL TYPE ORGANIC LINER SPECIFIC MATERIAL TYPE FIBER-REINFORCED POLYESTER ** DUCTWORK REHEATER TO STACK LOCATION SHELL GENERIC MATERIAL TYPE STAINLESS STEEL SHELL SPECIFIC MATERIAL TYPE **AUSTENITIC** LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DUCTWORK LOCATION BYPASS/TRANSITION DUCT SHELL GENERIC MATERIAL TYPE CARBON STEEL SHELL SPECIFIC MATERIAL TYPE **AISI 1110** LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** REAGENT PREPARATION EQUIPMENT ИR FUNCTION DEVICE NR DEVICE TYPE NR ** TANKS SERVICE NUMBER -----2 ABSORBER RECYCLE SECONDARY REACTION 2 VACUUM FILTER FILTRATE 3 THICKENER OVERFLOW 1 REAGENT PREP PRODUCT ** PUMPS NUMBER SERVICE REACTOR TRANSFER 2

ABSORBER RECIRCULATION

LOUISVILLE GAS & ELECTRIC: CANE RUN 6 (CONT.)

THICKENER HOLD TANK TRANSFER	2
LIME SLURRY	2
SODA ASH SOLUTION PUMP	2
THICKENER UNDERFLOW	4
VACUUM	3
LIME SLURRY FEED	2
VACUUM FPUMP	****
FILTRATE SUMP	2
SODA ASH	2
SILENCER OVERFLOW SUMP	2

** SOLIDS CONCENTRATING/DEWATERING

VACUUM FILTER DEVICE NUMBER 3 NUMBER OF SPARES 1 CAPACTTY 3 TON/DAY STAINLESS STEEL SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE AUSTENITIC BELT SPECIFIC MATERIAL TYPE FIBER-REINFORCED POLYESTER 25% SOLIDS FEED STREAM CHARACTERISTICS 63% SOLIDS OUTLET STREAM CHARACTERISTICS

** SOLIDS CONCENTRATING/DEWATERING

DEVICE THICKENER
NUMBER 1
CONFIGURATION CYLINDRICAL
DIMENSIONS - FT 125.0 DIA X 23.0
SHELL GENERIC MATERIAL TYPE CARBON STEEL
OUTLET STREAM CHARACTERISTICS 25% SOLIDS

*** SLUDGE

** TREATMENT

METHOD FIXATION
DEVICE PROPRIETARY PROCESS FORWERSION SYSTEMS [POZ-O-TEC]

** DISPOSAL

NATURE FINAL
TYPE LANDFILL
LOCATION ON-SITE
SITE TRANSPORTATION METHOD TRUCK
SITE TREATMENT NONE

** PROCESS CONTROL AND INSTRUMENTATION

PHYSICAL VARIABLES

MONITOR LOCATION

PROCESS CONTROL MANNER

PROCESS CHEMISTRY MODE

** WATER BALANCE

WATER LOOP TYPE CLOSED EVAPORATION WATER LOSS - LITER/S 17.5 (278 GPM)

** FGD SPARE CAPACITY INDICES

ABSORBER - % 20.0 FAN - % .0 RECIRCULATION PUMP - % 100.0

** FGD SPARE COMPONENT INDICES

ABSORBER .3
FAN .0
RECIRCULATION PUMP 1.0

PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY (JTILIZATION	% RE1	10VAL PART.	PER HOURS	BOILER HOURS	FGD HOURS	CAP.
4/79	SYSTEM	67.0	49.9	49.0	32.9	92.00		720	475	237	37.0
	** PROB	LEMS/SOLUTIO	NS/COMMENTS								
			HIS UNIT STAR			4, 1979). CO	1PLIANO	E TEST	ING IS	
5/79	SYSTEM	46.0	21.5	21.0	14.7	91.00		744	506	109	42.0
6/79	SYSTEM	27.0	12.3	12.0	10.3	93.00		720	601	74	47.0
	** PROE	LEMS/SOLUTIO	NS/COMMENTS								
		ו ו	THE UTILITY RETHAT NO UNUSUATED IS NOW OUT	AL PROCESS PRO T OF SERVICE D	OBLEMS HAVE DUE TO THE	BEEN E	NCOUN	TERED.	HOMEA	ER THE	SYS-
7/79	SYSTEM		.0		.0			744	529	0	45.0
	** PROE	SLEMS/SOLUTIO	NS/COMMENTS								
			THE UNIT DID N MIST ELIMINATO		N JULY AS P	ROCEDUF	RES CO	AT I NUEI	TO RE	PLACE 7	THE
8/79	SYSTEM	10.0	7.0	7.0	7.0			744	683	51	51.0
9/79	SYSTEM	70.0	60.0	60.0	44.0			720	531	317	46.0
	** PROE	BLEMS/SOLUTIO	ONS/COMMENTS								
		i	DURING AUGUST FAILURE OF FIND DFF OF THE SHA	/E PUMPS. THI							
0/79	SYSTEM	96.0	81.4	81.0	28.9			744	246	215	37.0
.1/79	SYSTEM	96.0	97.7	97.0	63.5			720	468	457	41.0
2/79	SYSTEM	98.0	94.9	95.0	89.7			744	703	667	60.0
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS								
			THE UTILITY RI QUARTER OF 19							E FOUR	тн
1/80	SYSTEM	86.0	49.0	49.0	13.8			744	210	103	32.0
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS								
		•	FGD SYSTEM OU' THE RAKE BECAI TO BE CLEANED	ME INOPERABLE	JANUARY WAS BECAUSE OF	CAUSE HIGH	D BY A SOLIDS	THICK AND T	ENER FA HE THIC	ILURE. KENER	HAD
2/80	SYSTEM	91.0	84.7	84.0	47.0			696	386	327	37.0
3/80	SYSTEM	72.0	70.0	70.0	64.5			744	686	480	51.0
	** PROE	SLEMS/SOLUTION	DNS/COMMENTS								
			IN FEBRUARY AN PUMPS.	ND MARCH OUTA	GE TIME WAS	CAUSE	BY P	ROBLEM	S WITH	THE RE	CYCLE

4/80 SYSTEM 98.8 91.5

97.7 73.9

720 581 531 37.0

LOUISVILLE GAS & ELECTRIC: CANE RUN 6 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER OUTAGES IN APRIL WERE A RESULT OF THE LOSS OF ONE OF THE BOILER FEED PUMPS AND BECAUSE THE LOAD WAS NOT NEEDED.

THE FGD OUTAGES WERE A RESULT OF HIGH BOOSTER FAN SUCTION TRIPS, REPAIRS TO THE IUCS SYSTEM, REPAIRS TO THE THICKENER UNDERFLOW LINE AND A PLANNED INSPECTION OF THE TRAYS. THE TRAY PLUGGING PROBLEM WAS SOLVED BY A SLIGHT PH ADJUSTMENT IN THE REACTORS.

5/80 SYSTEM 99.9 99.9 99.5 744 741 740 52.0

** PROBLEMS/SOLUTIONS/COMMENTS

DURING MAY THE PRESSURE RELIEF VALVE ON THE BOOSTER FAN MALFUNCTIONED FORCING THE FGD SYSTEM OUT OF SERVICE.

6/80 SYSTEM 99.9 99.7 99.9 88.9 72**0** 642 640 50.0

** PROBLEMS/SOLUTIONS/COMMENTS

A SPRAY PUMP MALFUNCTION CAUSED THE SYSTEM TO SHUTDOWN. APPROXIMATELY ONE HOUR WAS NEEDED TO PUT THE SPARE INTO SERVICE.

THE BOILER WAS OFF FOR REPAIRS TO THE CLINKER GRINDER AND TO REPAIR A BOILER TUBE LEAK.

IMPROVEMENTS TO THE PH CONTROL CIRCUITRY HAVE LEAD TO IMPROVED CARBIDE LIME UTILIZATION.

EXPERIMENTATION WITH A NEW FILTER CLOTH HAS SHOWN AN IMPROVEMENT IN SODA ASH CONSUMPTION.

SULFUR DIOXIDE EMISSIONS AVERAGED LESS THAN 200 PPM FOR JUNE.

7/80 SYSTEM 99.9 99.7 99.9 82.9 744 618 617 52.0

** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE PERIOD FROM JULY 17 THROUGH JULY 28 AN ACCEPTANCE TEST WAS RUN. DURING THE TEST THE FGD SYSTEM EXPERIENCED NO MAJOR PROBLEMS OR OUTAGE TIME. THE AVERAGE SO2 REMOVAL EFFICIENCY DURING THE TEST WAS 93.9%.

DURING NORMAL OPERATION IN JULY NO MAJOR FGD RELATED PROBLEMS WERE ENCOUNTERED.

8/80 SYSTEM 99.3 94.6 94.6 84.5 628 50.0 744 665 9/80 SYSTEM 94.0 98.6 98.7 626 50.0 86.9 720 635

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR PROBLEMS OCCURRED DURING THE MONTHS OF AUGUST AND SEPTEMBER.

10/80 SYSTEM 99.8 99.8 99.8 99.8 744 743 743 33.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR PROBLEMS OCCURRED DURING THE MONTHS OF

11/80 SYSTEM 85.1 96.8 96.8 55.1 720 409 397 33.0

	MODULE AVA	ILABILI	TY OPERABILITY R	RELIABILITY	UTILIZATION	% REN	10VAL PART.	PER HOURS	BOILER HOURS	FGD HOURS	
			IONS/COMMENTS								
			DURING OCTOBER PROBLEMS WERE E			Y REPO	RTED	THAT NO	MAJOR	FGD-RE	ELATED
12/80	SYSTEM	60.0	6.0	6.0	1.9			744	240	14	50.0
	** PROBLEM	S/SOLUT	IONS/COMMENTS								
			DURING DECEMBER TO SHUTDOWN FOR				SHEA	RED-OFF	CAUSI	NG THE	SYSTEM
1/81	SYSTEM	85.7	83.3	83.3	80.2			744	716	597	50.0
	** PROBLEM	S/SOLUT	IONS/COMMENTS								
			DURING JANUARY OUTAGE TIME.	PROBLEMS WI	тн тне тніск	ENER F	ACK S	HAFT CO	NTINUE	TO CA	USE
2/81	SYSTEM	99.6	99.5	99.5	71.6			672	483	481	45.0
	** PROBLEM	S/SOLUT	IONS/COMMENTS								
			DURING FEBRUARY		Y REPORTED T	HAT NO	MAJO	R FGD-R	ELATED	PROBLE	MS
3/81	SYSTEM	99.6	34.2	34.2	28.0			744	607	208	50.0
	** PROBLEM	S/SOLUT	IONS/COMMENTS								
			DURING MARCH OU	JTAGE TIME W	IAS DUE TO ST	RIKING	WORK	ERS AT	THE PL	ANT.	
4/81	SYSTEM	95.0	98.5	100.0	82.6			720	604	595	45.0
5/81	SYSTEM	96.8	96.9	100.0	96.8			744	243	720	55.0
6/81	SYSTEM	88.9	100.0	100.0	26.5			720	191	191	45.0
	** PROBLEM	s/solut	IONS/COMMENTS								
			THE UTILITY REP			-RELAT	red pr	OBLEMS	WERE E	NCOUNTE	RED
7/81	SYSTEM	74.0	69.0	69 .0	57.0			744	615	424	50.0
8/81	SYSTEM	80.0	73.0	77.0	68.0			744	693	506	50.0
9/81	SYSTEM	100.0	98.0	98.0	22.0			720	162	158	50.0
	** PROBLEM	S/SOLUT	IONS/COMMENTS								
			RUPTURE OF THE THE THIRD QUAR' IN OCTOBER FOR	TER 1981. TH	KE UNIT IS EX	KPECTE) TO B	IPE CAU E REMOV	JSED PR VED FRO	OBLEMS M SERV:	DURING ICE
10/81	SYSTEM	100.0			.0			720	0	0	.0
11/81	SYSTEM	100.0			.0			720	0	0	.0
12/81	SYSTEM	100.0			.0			744	0	0	.0

LOUISVILLE GAS & ELECTRIC: CANE RUN 6 (CONT.)

				DEBEORKY	ICE DATA					
PERIOD		AVAILABILITY	OPERABILITY		UTILIZATION	% REMOVAL SO2 PART.	PER	BOILER	FGD	CAP.
*****	** PROE	BLEMS/SOLUTION								
				JRTH QUARTER	THE BOILER &	IAS DOWN FOR	A TURE	BINE OVE	ERHAUL.	
1/82	SYSTEM	100.0	83.5	83.5	21.9		744	195	163	17.0
2/82	SYSTEM	100.0	76.5	76.5	70.4		672	618	473	54.0
3/82	SYSTEM	100.0	93.8	93.8	68.7		744	545	511	44.0
	** PROB	BLEMS/SOLUTION	NS/COMMENTS							
				PORTED THAT		-RELATED PRO	BLEMS	WERE EN	NCOUNTE	ERED
4/82	SYSTEM	100.0	99.6	100.0	68.2		720	493	491	50.0
5/82	SYSTEM	100.0	99.7	100.0	96.4		744	719	717	50.0
6/82	SYSTEM	98.6	98.3	100.0	82.6		720	605	595	50.0
	** PROE	BLEMS/SOLUTION	NS/COMMENTS							
			· · - · - · · · · · · · · · · · · · · · · · ·	EPORTED THAT		-RELATED PRO	BLEMS	WERE EN	NCOUNTE	ERED
7/82	SYSTEM	15.2	17.1	17.1	15.2		744	661	113	50.0
8/82	SYSTEM	42.6	50.6	50.6	42.6		744	626	317	50.0
9/82	SYSTEM	60.6	86.5	86.5	60.6		720	504	436	50.0
10/82	SYSTEM	87.0	94.9	94.9	87.0		744	682	647	50.0
11/82	SYSTEM	68.6	99.8	99.8	68.6		720	495	494	50.0
12/82	SYSTEM	62.9	95.1	95.1	62.9		744	492	468	50.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS							
				EPORTED THAT Y THROUGH DEC		NATOR COLLAR	SED DI	JRING TH	ΗE	
1/83	SYSTEM	52.8	99.7	99.7	52.8		744	394	393	50.0
2/83	SYSTEM	.0			.0		672	0	0	50.0
3/83	SYSTEM	.0			.0		744	0	0	50.0
4/83	SYSTEM	3.3	12.0	12.0	3.3		720	200	24	50.0
5/83	SYSTEM	32.1	51.6	51.6	32.1		744	463	239	50.0
6/83	SYSTEM	38.3	52.6	52.6	38.3		720	525	276	50.0

** PROBLEMS/SOLUTIONS/COMMENTS

A TURBINE OVERHAUL WAS PERFORMED DURING THE PERIOD OF JANUARY THROUGH JUNE 1983 ACCOUNTING FOR SOME OF THE OUTAGE TIME DURING THAT PERIOD.

THE FAILURE OF A BOOSTER FAN ACCOUNTED FOR OUTAGE TIME DURING THE PERIOD OF JANUARY THROUGH JUNE 1983.

7/83 SYSTEM 80.2 95.1 95.1 80.4 744 629 598 50.0

720

				PERFORMAN	CE DATA						
PERIOD	MODULE	AVAILABILITY		RELIABILITY		S 02			BOILER HOURS		
8/83	SYSTEM	39.5	43.6	43.6	39.5			744	675	294	50.0
9/83	SYSTEM	89.9	84.5	84.5	40.3			720	343	290	50.0
	** PRO	BLEMS/SOLUTION	NS/COMMENTS								
		s	LURRY PIPING	REPAIRS WERE	MADE DURING	THE '	THIRD	QUARTER	OF 198	33.	
10/83	SYSTEM	60.8	93.2	93.2	40.3			744	322	300	
11/83	SYSTEM	92.4	100.0	100.0	7.1			720	51	51	
12/83	SYSTEM	64.5	50.2	50.2	16.5			744	245	123	
	** PRO	BLEMS/SOLUTION	NS/COMMENTS								
		N	O MAJOR FGD-I	RELATED PROBL	EMS WERE REP	ORTED	FOR T	HE FOUR	RTH QUAR	RTER OF	1983.
1/84	SYSTEM							744			
2/84	SYSTEM							6 96			
3/84	SYSTEM							744			
4/84	SYSTEM							720			
5/84	SYSTEM							744			
6/84	SYSTEM							720			
7/84	SYSTEM							744			
8/84	SYSTEM							744			

^{**} PROBLEMS/SOLUTIONS/COMMENTS

9/84 SYSTEM

INFORMATION WAS UNAVAILABLE FOR THE FIRST THREE QUARTERS OF 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

LOUISVILLE GAS & ELECTRIC COMPANY NAME MILL CREEK PLANT NAME UNIT NUMBER LOUISVILLE CITY KENTUCKY STATE 43. 516. ***** 1084 REGULATORY CLASSIFICATION (.100 LB/MMBTU) (1.200 LB/MMBTU) (****** LB/MMBTU) PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW 358 334 339 358 GROSS UNIT GENERATING CAPACITY - MW NET UNIT GENERATING CAPACITY W/FGD - MW
NET UNIT GENERATING CAPACITY WO/FGD - MW EQUIVALENT SCRUBBED CAPACITY - MM ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER COMBUSTION ENGINEERING PULVERIZED COAL BOILER TYPE BOILER SERVICE LOAD BASE DESIGN BOILER FLUE GAS FLOW - CU.M/S BOILER FLUE GAS TEMPERATURE - C 660.66 (1400000 ACFM) 151.7 (305 F) 183. (600 FT) STACK HEIGHT - M CONCRETE STACK SHELL STACK TOP DIAMETER - M 5.8 (19.0 FT) ** FUEL DATA FUEL TYPE COAL BITUMINOUS FUEL GRADE 26749. AVERAGE HEAT CONTENT - J/G (11500 BTU/LB) RANGE HEAT CONTENT - BTU/LB 10800-12100 14.50 AVERAGE ASH CONTENT + % 10.0-18.0 RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - % 9.00 RANGE MOISTURE CONTENT - % 8.0-10.0 AVERAGE SULFUR CONTENT - % 3.75 3.75 3.5-4.5 RANGE SULFUR CONTENT - %
AVERAGE CHLORIDE CONTENT - % .04 RANGE CHLORIDE CONTENT % .03-.06 *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER ٥ TYFE NONE ** FABRIC FILTER NUMBER Λ TYPE NONE ** ESP NUMBER 2 NUMBER OF SPARES 0 HOT SIDE SUPPLIER WESTERN PRECIPITATOR INLET FLUE GAS CAPACITY - CU.M/S
INLET FLUE GAS TEMPERATURE - C 330.3 (700000 ACFM) 151.7 (305 F) (1. IN-H20) .1 99.4 PRESSURE DROP - KPA PARTICLE REMOVAL EFFICENCY - % ** PARTICLE SCRUBBER NUMBER 0 GENERIC TYPE NONE SPECIFIC TYPE TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL SHELL SPECIFIC MATERIAL N/A LINER GENERIC MATERIAL N/A

N/A

LINER SPECIFIC MATERIAL

*** FGD SYSTEM

```
** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                            THROWAWAY PRODUCT
   SO2 REMOVAL MODE
                                             WET SCRUBBING
   PROCESS TYPE
                                             LIME
   PROCESS ADDITIVES
                                             NONE
   SYSTEM SUPPLIER
                                             COMBUSTION ENGINEERING
   A-E FIRM
                                             FLUOR - PIONEER
   DEVELOPMENT LEVEL
                                             FULL SCALE
   NEW/RETROFIT
                                             RETROFIT
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.50
   UNIT DESIGN SO2 REMOVAL EFFICIENCY ~ %
                                                85.00
   ENERGY CONSUMPTION - %
   CURRENT STATUS
                                              1
   COMMERCIAL START-UP
                                              4/81
   INITIAL START-UP
                                             12/80
   CONTRACT AWARDED
                                             11/77
** DESIGN AND OPERATING PARAMETERS
   DESIGN COAL SULFER CONTENT %
                                                 4.50
   DESIGN COAL HEAT CONTENT - J/G
                                            23260.0
                                                           ( 10000 BTU/LB)
   DESIGN COAL ASH CONTENT - %
                                              18.00
   DESIGN MOISTURE CONTENT - %
                                                10.00
   DESIGN CHLORIDE CONTENT - %
                                                 .06
   OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                              120.0
** QUENCHER/PRESATURATOR
   NUMBER
                                              0
                                             NONE
   TYPE
** ABSORBER
   NUMBER
                                              2
   NUMBER OF SPARES
                                              Ω
   GENERIC TYPE
                                             SPRAY TOWER
                                             OPEN COUNTERCURRENT SPRAY
   SPECIFIC TYPE
   TRADE NAME/COMMON TYPE
                                             N/A
                                             COMBUSTION ENGINEERING
   SUPPLIER
                                             26.0 X 31.0
   DIMENSIONS FT
   SHELL GENERIC MATERIAL
                                             STAINLESS STEEL
   SHELL SPECIFIC MATERIAL
                                             AUSTENITIC
   SHELL MATERIAL TRADE NAME/COMMON TYPE
                                            TYPE 316L
                                             NONE
   LINER GENERIC MATERIAL
   LINER SPECIFIC MATERIAL
                                             N/A
   LINER MATERIAL TRADE NAME/COMMON TYPE
                                             N/A
   NUMBER OF CONTACTING ZONES
   LIQUID RECIRCULATION RATE - LITER/S
                                              3755.
                                                          (59600 GPM)
                                              11.9
   L/G RATIO - L/CU.M
                                                           ( 88.9 GAL/1000 ACF)
                                                3.7
                                                           ( 12.0 FT/S)
   SUPERFICAL GAS VELOCITY - M/SEC
   INLET GAS FLOH - CU. M/S
                                               316.17
                                                           ( 670000 ACFM)
                                               148.9
                                                           ( 300 F)
   INLET GAS TEMPERATURE C
   SO2 REMOVAL EFFICIENCY - %
                                                86.6
** REHEATER
                                              2
   NUMBER
                                              0
   NUMBER OF SPARES
   NUMBER PER MODULE
                                              1
                                             IN-LINE
   GENERIC TYPE
                                             STEAM
   SPECIFIC TYPE
                                             FIN TUBE
   TRADE NAME/COMMON TYPE
                                             DOWNSTREAM OF ABSORBER
   LOCATION
                                             27.8 ( 50 F)
   TEMPERATURE INCREASE - C
                                                            ( 130 F)
   INLET FLUE GAS TEMPERATURE C
                                                54.4
                                               82.2
   OUTLET FLUE GAS TEMPERATURE - C
                                                           ( 180 F)
   NUMBER OF HEAT EXCHANGER BANKS
                                                2
   CONSTRUCTION MATERIAL GENERIC TYPE
                                            CARBON STEEL
                                          AISI 1110
   CONSTRUCTION MATERIAL SPECIFIC TYPE
```

××	FANS	
	NUMBER	2
	NUMBER OF SPARES	0
	DESIGN	CENTRIFUGAL
		AMERICAN STANDARD
	SUPPLIER	
	FUNCTION	BOOSTER
	APPLICATION	INDUCED DRAFT
	SERVICE	DRY
	FLUE GAS TEMPERATURE - C	82.2 (180 F)
	CONSTRUCTION MATERIAL GENERIC TYPE	NR
	CONSTRUCTION TRIERIAL GENERIC TITE	TIR
**	FANS	
	NUMBER	2
	NUMBER OF SPARES	0
	DESIGN	CENTRIFUGAL
	SUPPLIER	AMERICAN STANDARD
	FUNCTION	UNIT
	APPLICATION	FORCED DRAFT
	SERVICE	DRY
	FLUE GAS FLOW RATE - CU.M/S	316.17 (670000 ACFM)
	FLUE GAS TEMPERATURE - C	148.9 (300 F)
	CONSTRUCTION MATERIAL GENERIC TYPE	NR
	CONSTRUCTION HATERIAL BENERIC TIFE	IIK
**	DAMPERS	
	NUMBER	2
	FUNCTION	SHUT-OFF
	GENERIC TYPE	LOUVER
	SPECIFIC TYPE	
		PARALLEL BLADE MULTILOUVER
	MANUFACTURER	COMBUSTION ENGINEERING
	MODULATION	OPEN/ CLOSED
	SEAL AIR FLOW - CU. M/S	.71 (1500 ACFM)
	CONSTRUCTION MATERIAL GENERIC TYPE	CARBON STEEL [BLADES & FRAMES]; STAINLESS STEEL
	CONSTRUCTION MATERIAL SPECIFIC TYPE	AISI 1110; AUSTENITIC
	LINER GENERIC MATERIAL TYPE	
		NONE
	LINER SPECIFIC MATERIAL TYPE	N/A
××	DAMPERS	
	NUMBER	2
	FUNCTION	SHUT-OFF
	GENERIC TYPE	
		LOUVER
	SPECIFIC TYPE	PARALLEL BLADE MULTILOUVER
	MANUFACTURER	COMBUSTION ENGINEERING
	MODULATION	OPEN/ CLOSED
	SEAL AIR FLOW CU. M/S	.71 (1500 ACFM)
	CONSTRUCTION MATERIAL GENERIC TYPE	CARBON STEEL [BLADES & FRAMES]; STAINLESS STEEL
	CONSTRUCTION MATERIAL SPECIFIC TYPE	
		AISI 1110; AUSTENITIC
	LINER GENERIC MATERIAL TYPE	NONE
	LINER SPECIFIC MATERIAL TYPE	N/A
××	DAMPERS	
	NUMBER	2
	FUNCTION	
		SHUT-OFF
	GENERIC TYPE	LOUVER
	SPECIFIC TYPE	PARALLEL BLADE MULTILOUVER
	MANUFACTURER	COMBUSTION ENGINEERING
	MODULATION	OPEN/ CLOSED
	SEAL AIR FLOW - CU. M/S	
	CONSTRUCTION MATERIAL GENERIC TYPE	
	CONSTRUCTION MATERIAL GENERIC TIPE	CARBON STEEL [BLADES & FRAMES]; STAINLESS STEEL
	CONSTRUCTION MATERIAL SPECIFIC TYPE	AISI 1110; AUSTENITIC
	LINER GENERIC MATERIAL TYPE	NONE
	LINER SPECIFIC MATERIAL TYPE	N/A
**	DUCTWOFK	
	LOCATION	ABSORBER INLET
	CONFIGURATION	RECTANGULAR
	SHELL GENERIC MATERIAL TYPE	CARBON STEEL
	SHELL SPECIFIC MATERIAL TYPE	AISI 1110
	LINER GENERIC MATERIAL TYPE	
	ITNED SPECIFIC MATERIAL TIPE	NR
	LINER SPECIFIC MATERIAL TYPE	NR

NR

**	DUCTWORK LOCATION CONFIGURATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	ABSORBER OUTLET RECTANGULAR CARBON STEEL AISI 1110 NR NR
**	DUCTWORK LOCATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	BYPASS CARBON STEEL AISI 1110 NONE N/A
**	REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE DEVICE TYPE NUMBER NUMBER OF SPARES PRODUCT QUALITY - % SOLIDS	WET BALL MILL COMPARTMENTED TUBE MILL 1 0
**	TANKS SERVICE ABSORBER RECYCLE REAGENT FEED	NUMBER 1 1
**	PUMPS SERVICE ABSORBER RECIRCULATION	NUMBER 8
**	SOLIDS CONCENTRATING/DEWATERING DEVICE NUMBER NUMBER OF SPARES CONFIGURATION DIMENSIONS - FT CAPACITY SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE BELT GENERIC MATERIAL TYPE BELT SPECIFIC MATERIAL TYPE BELT SPECIFIC MATERIAL TYPE FEED STREAM SOURCE FEED STREAM CHARACTERISTICS OUTLET STREAM CHARACTERISTICS OUTLET STREAM DISPOSITION	THICKENER 1 0 CIRCULAR 140 DIA X 15.0 1050000 GAL NR NR NR NR NR NR 120 GPM/10% SOLIDS 280 GPM/30% SOLIDS 840 GPM VACUUM FILTER
**	SOLIDS CONCENTRATING/DEWATERING DEVICE NUMBER NUMBER OF SPARES CONFIGUPATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE BELT GENERIC MATERIAL TYPE BELT GENERIC MATERIAL TYPE BELT SPECIFIC MATERIAL TYPE BELT SPECIFIC MATERIAL TYPE FEED STREAM SOURCE FEED STREAM CHARACTERISTICS OUTLET STREAM CHARACTERISTICS OUTLET STREAM DISPOSITION	VACUUM FILTER 5 1 CIRCULAR NR NR NR NR NR THICKENER UNDERFLOW 25% SOLIDS PUG MILL

LOUISVILLE GAS & ELECTRIC: MILL CREEK 1 (CONT.)

*** SALEABLE BYPRODUCTS

NONE NATURE

*** SLUDGE

** TREATMENT

FIXATION METHOD PUG MILL DEVICE

CONVERSION SYSTEMS [POZ-O-TEC] PROPRIETARY PROCESS

INLET QUALITY - % 45.0

** DISPOSAL

FINAL NATURE LANDFILL TYPE DN-SITE LOCATION SITE TRANSPORTATION METHOD TRUCK CLAY LINING SITE TREATMENT

10 SITE SERVICE LIFE - YRS

** WATER BALANCE

OPEN/CLOSED WATER LOOP TYPE

(1984 GPM) MAKEUP WATER ADDITION - LITERS/S 125.0

** CHEMICALS AND CONSUMPTION

ABSORBENT FUNCTION CARBIDE LIME NAME PRINCIPAL CONSTITUENT 90% CAOH2 SOURCE/SUPPLIER AIRCO RECYCLE TANK POINT OF ADDITION

** FGD SPARE CAPACITY INDICES

ABSORBER - % .0 .0 MIST ELIMINATOR - % REHEATER - % .0 .0 FAN - % BALL MILL - % .0 .0 EFFLUENT HOLD TANK - % THICKENER - X .0 VACUUM FILTER - % .0

** FGD SPARE COMPONENT INDICES

.0 ABSOPBER MIST ELIMINATOR . 0 REHEATER . 0 FAN .0 BALL MILL .0 EFFLUENT HOLD TANK .0 THICKENER .0 VACUUM FILTER .0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

12/80 SYSTEM 45.2 98.5 98.5 44.5 90.00 744 336 331 60.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM IS PRESENTLY IN THE STARTUP PHASE. OPERATIONS BEGAN ON DECEMBER 17, 1980 AND NO MAJOR PROBLEMS WERE REPORTED.

1/81 SYSTEM 51.0 46.0 46.0 42.0 94.80 744 675 312 45.0

				PERFORMANO	E DATA					
PERIOD				RELIABILITY U		SO2 PART.	HOURS	HOURS	HOURS	FACTOR
		BLEMS/SOLUTION								
	AA FROL			, A DEOKEN BL			C C41101		/TMATE!	V 747
			OURS OF OUTAG	A BROKEN BLE SE TIME.	ED PUMP DIS	CHARGE LINE	5 CAUSI	E APPRU	KTUWIEL	.1 303
2/81	SYSTEM	51.5	51.5	51.5	51.5		672	346	346	50.0
3/81	SYSTEM	39.0	36.0	36.0	35.0		744	712	258	50.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS							
			URING FEBRUAF	RY AND MARCH I	PROBLEMS WER	E ENCOUNTER	ED DUE	то тне	THICKE	ENER
			DDITIONAL OU LANT.	TAGE TIME DUR	ING MARCH WA	S DUE TO ST	RIKING	WORKER:	S AT TH	łE
4/81	SYSTEM	39.9	25.2	25.2	7.9		720	226	57	25.0
5/81	SYSTEM	46.9	60.7	60.7	21.8		744	267	162	35.0
6/81	SYSTEM	56.1	33.9	33.9	26.5		720	563	191	50.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS							
		-		COND QUARTER		LITY REPORT	ED HAV	ING PRO	BLEMS	
7/81	SYSTEM	76.3	75.3	75.3	72.2		744	713	537	65.0
8/81	SYSTEM	99.2	99.2	99.2	98.7		744	740	734	65.0
9/81	SYSTEM	85.7	95.5	95.5	79.6		720	600	573	60.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS							
		A	ALL FGD SYSTE	M DOWNTIME DU THE GLYCOL H	RING THE THI EAT EXCHANGE	RD QUARTER	1981 W.	AS ATTR YSTEM.	IBUTED	то
10/81	SYSTEM	39.6	41.0	41.0	39.6		720	719	295	50.0
11/81	SYSTEM	37.4	39.8	39.8	37.4		720	675	269	50.0
12/81	SYSTEM	26.1	29.1	29.1	26.1		744	666	194	50.0

** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE FOURTH QUARTER PROBLEMS WERE ENCOUNTERED WITH THE GLYCOL HEAT EXCHANGER.

1/82	SYSTEM	4.7	6.2	6.2	4.7	744	570	36	50.0
2/82	SYSTEM	25.4	25.6	25.6	25.4	672	669	171	50.0
3/82	SYSTEM	41.3	54.9	54.9	41.3	744	560	307	50.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT FROZEN LINES DURING THE FIRST QUARTER 1982 HINDERED THE FGD SYSTEM OPERATION.

AN ADDITIONAL PROBLEM EXPERIENCED DURING THE PERIOD WAS HEAT EXCHANGER FAILURE.

PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% REMOVAL SO2 PART.	PER HOURS	BOILER HOURS	FGD HOURS	CAP.
4/82	SYSTEM	96.4	63.9	63.9	6.4		720	72	46	50.0
5/82	SYSTEM	43.1	35.2	35.2	30.9		744	653	230	50.0
6/82	SYSTEM	77.9	42.2	42.2	16.2		720	277	117	50.0
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
			DURING THE SEC		MAJOR PROBLE	MS WERE EXF	PERIENC	ED WITH	THE G	YCOL
7/82	SYSTEM	33.5	61.5	61.5	23.4		744	283	174	50.0
8/82	SYSTEM	64.5	69.7	69.7	64.5		744	689	480	50.0
9/82	SYSTEM	75.3	75.3	75.3	75.3		720	720	542	50.0
	** PRO	BLEMS/SOLUTIO	DNS/COMMENTS							
			THE UTILITY REDURING THE MOS					T SYSTE	M OCCUF	RED
10/82	SYSTEM	47.3	49.4	49.4	47.3		744	712	352	50.0
11/82	SYSTEM	83.8	83.8	83.8	83.8		720	720	603	50.0
12/82	SYSTEM	21.2	38.6	38.6	21.2		744	409	158	50.0
	** PRO	BLEMS/SOLUTIO	DNS/COMMENTS							
			THE UTILITY RIDURING THE PER				CAUSED	SOME O	UTAGE '	TIME
			SPRAY PUMP PRO DECEMBER 1982		ALSO REPORTED	FOR THE PE	RIOD O	F JULY	THROUG	1
1/83	SYSTEM	40.9	43.7	43.7	40.9		744	695	304	50.0
2/83	SYSTEM	47.2	47.1	47.1	47.0		672	671	316	50.0
3/83	SYSTEM	77.2	85.6	85.6	76.5		744	665	569	50.0
4/83	SYSTEM	43.9	82.1	82.1	43.9		720	385	316	50.0
5/83	SYSTEM	9.7	19.3	19.3	9.7		744	374	72	50.0
6/83	SYSTEM	55.0	62.8	62.8	55.0		720	631	396	50.0
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS							
			THE UTILITY RIDURING THE PE				ACCOU	NTED FO	R OUTA	GE TIME
7/83	SYSTEM	56.2	57.4	57.4	55.5		744	719	413	50.0
8/83	SYSTEM	48.0	48.4	48.4	48.0		744	737	357	50.0
9/83	SYSTEM	44.7	35.0	35.0	24.6		720	505	177	50.0

PERFORMANCE DATA						
PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION	% REN	10VAL	PER	BOILER	FGD	CAP.
	S02	PART.	HOURS	HOURS	HOURS	FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

STACK REHEAT FAILURES DURING THE PERIOD RESULTED IN A STACK PLUME REHEAT SYSTEM DESIGN.

10/83	SYSTEM	82.4	79.3	79.3	66.4	744	623	494
11/83	SYSTEM	73.3	68.4	68.4	56.8	720	598	409
12/83	SYSTEM	58.2	46.3	46.3	39.2	744	630	292

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE REPORTED FOR THE FOURTH QUARTER OF 1983.

1/84	SYSTEM	744
2/84	SYSTEM	696
3/84	SYSTEM	744
4/84	SYSTEM	720
5/84	SYSTEM	744
6/84	SYSTEM	720
7/84	SYSTEM	744
8/84	SYSTEM	744
9/84	SYSTEM	720

^{**} PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE FIRST THREE QUARTERS OF 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COMPANY NAME PLANT NAME UNIT NUMBER CITY STATE REGULATORY CLASSIFICATION	LOUISVILLE GAS & ELECTRIC MILL CREEK 2 LOUISVILLE KENTUCKY E
PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW NET UNIT GENERATING CAPACITY W/FGD - MW NET UNIT GENERATING CAPACITY W/FGD - MW EQUIVALENT SCRUEBED CAPACITY - MW	43. (.100 LB/MMBTU) 516. (1.200 LB/MMBTU) ****** (****** LB/MMBTU) ***** 350 325 330 350
** UNIT DATA - BOILER AND STACK BOILER SUPPLIER EOILER TYPE BOILER SERVICE LOAD DESIGN BOILER FLUE GAS FLOW - CU.M/S BOILER FLUE GAS TEMPERATURE - C STACK HEIGHT - M STACK SHELL STACK TOP DIAMETER - M	COMBUSTION ENGINEERING PULVERIZED COAL BASE 660.66 (1400000 ACFM) 151.7 (305 F) 183. (600 FT) CONCRETE 5.8 (19.0 FT)
** FUEL DATA FUEL TYPE FUEL GRADE AVERAGE HEAT CONTENT - J/G RANGE HEAT CONTENT - BTU/LB AVERAGE ASH CONTENT - % RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - % AVERAGE MOISTURE CONTENT - % AVERAGE SULFUR CONTENT - % RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - %	COAL BITUMINOUS 26749. (11500 BTU/LB) 10800-12100 14.50 10.0-18.0 9.00 8.0-10.0 3.75 3.5-4.5 .04 .0306
*** PARTICLE CONTROL	
** MECHANICAL COLLECTOR NUMBER TYPE	0 NONE
** FABRIC FILTER NUMBER TYPE	0 NONE
** ESP NUMBER NUMBER OF SPARES TYPE SUPPLIER PRESSURE DROP - KPA PARTICLE REMOVAL EFFICENCY - %	2 0 HOT SIDE WESTERN PRECIPITATOR .1 (1. IN-H20) 99.4
** PARTICLE SCRUBBER NUMBER GENERIC TYPE SPECIFIC TYPE TRADE NAME/COMMON NAME SHELL GENEPIC MATERIAL SHELL SFECIFIC MATERIAL LINER GENERIC MATERIAL LINER SPECIFIC MATERIAL	0 NONE N/A N/A N/A N/A

*** FGD SYSTEM

```
** GENERAL DATA
  SALEABLE PRODUCT/THROWAWAY PRODUCT
                                             THROWAWAY PRODUCT
   SO2 REMOVAL MODE
                                              WET SCRUBBING
   PROCESS TYPE
                                              LIME
   PROCESS ADDITIVES
                                              NONE
   SYSTEM SUPPLIER
                                              COMBUSTION ENGINEERING
   A-E FIRM
                                              FLUOR - PIONEER
   DEVELOPMENT LEVEL
                                              FULL SCALE
                                              RETROFIT
   NEW/RETROFIT
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - 2 99.50
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                               85.00
   ENERGY CONSUMPTION - %
                                                  1.4
   CURRENT STATUS
                                               1
   COMMERCIAL START-UP
                                               4/82
   INITIAL START-UP
                                              12/81
                                              11/77
   CONTRACT AWARDED
** DESIGN AND OPERATING PARAMETERS
   DESIGN COAL SULFER CONTENT - %
                                                  4.50
   DESIGN COAL HEAT CONTENT - J/G
                                             23260.0
                                                             ( 10000 BTU/LB)
   DESIGN COAL ASH CONTENT - %
                                               18.00
   DESIGN MOISTURE CONTENT - Z
                                                 10.00
   DESIGN CHLORIDE CONTENT - %
                                                   .06
** QUENCHER/PRESATURATOR
                                              NONE
   TYPE
** ARSORRED
   NUMBER
                                               2
   NUMBER OF SPARES
                                               0
   GENERIC TYPE
                                              SPRAY TOWER
   SPECIFIC TYPE
                                              OPEN COUNTERCURRENT SPRAY
   TRADE NAME/COMMON TYPE
                                              N/A
   SUPPLIER
                                              COMBUSTION ENGINEERING
   DIMENSIONS - FT
                                              26.0 X 31.0
   SHELL GENERIC MATERIAL
                                              STAINLESS STEEL
                                              AUSTENITIC
   SHELL SPECIFIC MATERIAL
   SHELL MATERIAL TRADE NAME/COMMON TYPE
                                              TYPE 3161
   LINER GENERIC MATERIAL
                                              NONE
   LINER SPECIFIC MATERIAL
                                              N/A
   LINER MATERIAL TRADE NAME/COMMON TYPE
                                              N/A
   NUMBER OF CONTACTING ZONES
                                               4
                                                            (59600 GPM)
   LIQUID RECIRCULATION RATE - LITER/S
                                               3755.
                                                            ( 88.9 GAL/1000 ACF)
                                               11.9
   L/G RATIO L/CU.M
                                                            ( 12.0 FT/S)
   SUPERFICAL GAS VELOCITY - M/SEC
                                                  3.7
                                                316.17
   INLET GAS FLOW - CU. M/S
                                                             ( 670000 ACFM)
   INLET GAS TEMPERATURE - C
                                                148.9
                                                             ( 300 F)
   SO2 REMOVAL EFFICIENCY - %
                                                 86.6
** MIST ELIMINATOR
                                             PRIMARY COLLECTOR
   PRE-MIST ELIMINATOR/MIST ELIMINATOR
   NUMBER PER SYSTEM
                                               n
   NUMBER OF SPARES PER SYSTEM
   NUMBER PER MODULE
                                               2
                                              IMPINGEMENT
   GENERIC TYPE
   SPECIFIC TYPE
                                              BAFFLE
                                              CLOSED VANE
   TRADE NAME/COMMON TYPE
                                              ATLANTIC BRIDGE
   MANUFACTURER
                                              HORIZONTAL
   CONFIGURATION
   NUMBER OF STAGES
                                                  1
   NUMBER OF PASSES PER STAGE
                                                  3
                                                             ( .5 IN-H2O)
( 10.0 FT/S)
   PRESSURE DROP - KPA
                                                   .1
   SUPERFICAL GAS VELCCITY - M/S
                                                  3.0
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              NR
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              FRESH
   WASH WATER SOURCE
                                              INTERMITTENT
   WASH FREQUENCY
                                                 18.9
                                                             ( 300 GAL/MIN)
   WASH RATE - L/S
```

```
** REHEATER
   NUMBER
                                                 2
   NUMBER OF SPARES
                                                 0
   NUMBER PER MODULE
                                                 1
                                                IN-LINE
   GENERIC TYPE
    SPECIFIC TYPE
                                                STEAM
    TRADE NAME/COMMON TYPE
                                                FIN TUBE
    TEMPERATURE INCREASE - C
                                                   27.8
                                                                  50 F)
    OUTLET FLUE GAS TEMPERATURE - C
                                                   82.2
                                                                  180 F)
    NUMBER OF HEAT EXCHANGER BANKS
                                                   2
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                CARBON STEEL
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                AISI 1110
** FANS
                                                 2
   NUMBER
    NUMBER OF SPARES
                                                 0
                                                CENTRIFUGAL
    DESIGN
    SUPPLIER
                                                AMERICAN STANDARD
    FUNCTION
                                                ROOSTER
    APPLICATION
                                                INDUCED DRAFT
    SERVICE
                                                DRY
    FLUE GAS TEMPERATURE - C
                                                   82.2
                                                                ( 180 F)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                NR
** FANS
   NUMBER
                                                 2
    NUMBER OF SPARES
                                                 0
    DESIGN
                                                CENTRIFUGAL
    SUPPLIER
                                                AMERICAN STANDARD
    FUNCTION
                                                UNIT
    APPLICATION
                                                FORCED DRAFT
    SERVICE
                                                DRY
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                NR
** DAMPERS
   NUMBER
                                                 2
    FUNCTION
                                                SHUT-OFF
    GENERIC TYPE
                                                LOUVER
    SPECIFIC TYPE
                                                PARALLEL BLADE MULTILOUVER
    MANUFACTURER
                                                COMBUSTION ENGINEERING
   MODULATION
                                                OPEN/CLOSED
    SEAL AIR FLOW - CU. M/S
                                                     .71
                                                                    1500 ACFM)
                                                CARBON STEEL [BLADES & FRAMES]; STAINLESS STEEL
    CONSTRUCTION MATERIAL GENERIC TYPE
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                AISI 1110; AUSTENITIC
    LINER GENERIC MATERIAL TYPE
                                                NONE
    LINER SPECIFIC MATERIAL TYPE
                                                N/A
** DAMPERS
   NUMBER
                                                 2
    FUNCTION
                                                SHUT-OFF
    GENERIC TYPE
                                                LOUVER
    SPECIFIC TYPE
                                                PARALLEL BLADE MULTILOUVER
    MANUFACTURER
                                                COMBUSTION ENGINEERING
    MODULATION
                                                OPEN/CLOSED
    SEAL AIR FLOW - CU. M/S
                                                                    1500 ACFM)
                                                     .71
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                CARBON STEEL [BLADES & FRAMES]; STAINLESS STEEL
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                AISI 1110; AUSTENITIC
    LINER GENERIC MATERIAL TYPE
                                                NONE
    LINER SPECIFIC MATERIAL TYPE
                                                N/A
** DAMPERS
   NUMBER
                                                 2
    FUNCTION
                                                SHUT-OFF
    GENERIC TYPE
                                                LOUVER
   SPECIFIC TYPE
                                                PARALLEL BLADE MULTILOUVER
   MANUFACTURER
                                                COMBUSTION ENGINEERING
   MODULATION
                                                OPEN/CLOSED
    SEAL AIR FLOW - CU. M/S
                                                     .71
                                                                    1500 ACFM)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                                CARBON STEEL [BLADES & FRAMES]; STAINLESS STEEL
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                AISI 1110; AUSTENITIC
```

LINER GENERIC MATERIAL TYPE NONE
LINER SPECIFIC MATERIAL TYPE N/A

** DUCTWORK

LOCATION ABSORBER INLET
CONFIGURATION RECTANGULAR
SHELL GENERIC MATERIAL TYPE CARBON STEEL
SHELL SPECIFIC MATERIAL TYPE AISI 1110
LINER GENERIC MATERIAL TYPE NR
LINER SPECIFIC MATERIAL TYPE NR

** DUCTWORK

LOCATION ABSORBER OUTLET
CONFIGURATION RECTANGULAR
SHELL GENERIC MATERIAL TYPE NR
SHELL SPECIFIC MATERIAL TYPE NR
LINER GENERIC MATERIAL TYPE NR
LINER SPECIFIC MATERIAL TYPE NR

** DUCTWORK

LOCATION BYPASS
SHELL GENERIC MATERIAL TYPE CARBON STEEL
SHELL SPECIFIC MATERIAL TYPE AISI 1110
LINER GENERIC MATERIAL TYPE NONE
LINER SPECIFIC MATERIAL TYPE N/A

** REAGENT PREPARATION EQUIPMENT

FUNCTION WET BALL MILL
DEVICE COMPARTMENTED
DEVICE TYPE NR

** TANKS

SERVICE NUMBER
-----ABSORBER RECYCLE 1
REAGENT FEED 1

** PUMPS

SERVICE NUMBER

** SOLIDS CONCENTRATING/DEWATERING

THICKENER DEVICE 1 NUMBER 0 NUMBER OF SPARES CIRCULAR CONFIGURATION DIMENSIONS - FT 140 DIA X 15.0 1050000 GAL CAPACITY SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE NR LINER GENERIC MATERIAL TYPE NR LINER SPECIFIC MATERIAL TYPE N/A BELT GENERIC MATERIAL TYPE N/A BELT SPECIFIC MATERIAL TYPE ABSORBER BLEED FEED STREAM SOURCE 1120 GPM/10% SOLIDS FEED STREAM CHARACTERISTICS 280 GPM/30% SOLIDS OUTLET STREAM CHARACTERISTICS 840 GPM OVERFLOW STREAM CHARACTERISTICS VACUUM FILTER OUTLET STREAM DISPOSITION

** SOLIDS CONCENTRATING/DEWATERING

VACUUM FILTER DEVICE 1 NUMBER n NUMBER OF SPARES NR SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE NR NR LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE NR NR BELT GENERIC MATERIAL TYPE BELT SPECIFIC MATERIAL TYPE NR

LOUISVILLE GAS & ELECTRIC: MILL CREEK 2 (CONT.)

OUTLET STREAM CHARACTERISTICS 45% SOLIDS

*** SALEABLE BYPRODUCTS

NATURE NONE

*** SLUDGE

** TREATMENT

METHOD FIXATION
DEVICE PUG MILL

PROPRIETARY PROCESS CONVERSION SYSTEMS [POZ-0-TEC]

INLET QUALITY - % 45.0

** DISPOSAL

NATURE FINAL
TYPE LANDFILL
LOCATION ON-SITE
SITE TRANSPORTATION METHOD TRUCK
SITE TREATMENT CLAY LINING

SITE SERVICE LIFE - YRS 10

** WATER BALANCE

WATER LOOP TYPE CLOSED
MAKEUP WATER ADDITION - LITERS/S 125.0 (1984 GPM)

** FGD SPARE CAPACITY INDICES

ABSORBER - % .0

MIST ELIMINATOR - % .0

REHEATER - % .0

REHEATER - % .0
FAN - % .0
THICKENER - % .0
VACUUM FILTER - % .0

** FGD SPARE COMPONENT INDICES

ABSORBER .0
MIST ELIMINATOR .0
REHEATER .0
FAN .0
THICKENER .0

VACUUM FILTER .0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

12/81 SYSTEM 100.0 57.3 75.0 100.0 95.00 99.00 744 262 150 50.0

** PROBLEMS/SOLUTIONS/COMMENTS

MILL CREEK 2 COMMENCED OPERATIONS ON DECEMBER 18, 1981. THE FGD SYSTEM WAS AVAILABLE 100% OF THE TIME SINCE START-UP.

1/82 SYSTEM 24.1 25.3 25.3 24.1 744 707 179 50.0 2/82 SYSTEM 88.5 88.5 88.5 88.5 672 672 595 50.0 3/82 SYSTEM 73.8 73.8 73.8 73.8 744 744 549 50.0

** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE FIRST QUARTER 1982 THE UTILITY EXPERIENCED START-UP PROBLEMS WITH THE UNIT 2 FGD SYSTEM.

WITH THE UNIT 2 FGD SYSTEM

4/82 SYSTEM 85.6 84.1 100.0 75.7 720 648 545 50.0

	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% REM 502	OVAL PART.	PER HOURS	BOILER HOURS	FGD	
5/82	SYSTEM	100.0	100.0	100.0	22.4			744	167	167	50.0
6/82	SYSTEM	81.7	81.1	81.1	78.7			720	699	567	50.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			URING THE SE UTAGE TIME.	COND QUARTER	FAILURE OF T	HE REC	IRCULA	ATION F	PUMP CAL	JSED SC	ME
7/82	SYSTEM	.0	.0	.0	.0			744	714	0	50.0
8/82	SYSTEM	.0	.0	.0	.0			744	713	0	50.0
9/82	SYSTEM	.0	.0	.0	.0			720	558	0	50. 0
0/82	SYSTEM	.0	.0	.0	.0			744	739	0	50.0
1/82	SYSTEM	.0	.0	.0	.0			720	691	0	50.0
2/82	SYSTEM	55.8	70.1	70.1	50.4			744	535	375	50.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
					A MAJOR BEAR D OF JULY THR					OSTER F	MA
1/83	SYSTEM	36.8	38.6	38.6	36.8			744	710	274	50.0
-	SYSTEM SYSTEM			38.6 59.3				744 672			50.0 50.0
2/83		56.3	59.3		52.4				594	352	
2/83 3/83	SYSTEM	56.3 93.5	59.3 92.7	59.3	52.4 81.5			672	594 654	352 606	50.0
2/83 3/83 4/83	SYSTEM	56.3 93.5 86.8	59.3 92.7 87.2	59.3 92.7	52.4 81.5			672 744	594 654 555	352 606	50.0 50.0 50.0
2/83 3/83 4/83 5/83	SYSTEM SYSTEM SYSTEM	56.3 93.5 86.8	59.3 92.7 87.2	59.3 92.7 87.2	52.4 81.5 67.2			672 744 720	594 654 555 184	352 606 484	50.0 50.0 50.0
2/83 3/83 4/83 5/83	SYSTEM SYSTEM SYSTEM SYSTEM SYSTEM	56.3 93.5 86.8	59.3 92.7 87.2 .0	59.3 92.7 87.2	52.4 81.5 67.2			672 744 720 744	594 654 555 184	352 606 484	50.0 50.0 50.0
2/83 3/83 4/83 5/83	SYSTEM SYSTEM SYSTEM SYSTEM SYSTEM	56.3 93.5 86.8 .0 .0	59.3 92.7 87.2 .0 .0	59.3 92.7 87.2 .0	52.4 81.5 67.2	1S DURI	NG THI	672 744 720 744 720	594 654 555 184 151	352 606 484 0	50.0 50.0 50.0
2/83 3/83 4/83 5/83	SYSTEM SYSTEM SYSTEM SYSTEM SYSTEM	56.3 93.5 86.8 .0 .0 BLEMS/SOLUTIO	59.3 92.7 87.2 .0 .0 .sycomments the utility R through June	59.3 92.7 87.2 .0 EPORTED THICK	52.4 81.5 67.2 .0			672 744 720 744 720	594 654 555 184 151	352 606 484 0 0	50.0 50.0 50.0 50.0 50.0
2/83 3/83 4/83 5/83	SYSTEM SYSTEM SYSTEM SYSTEM SYSTEM	56.3 93.5 86.8 .0 .0 BLEMS/SOLUTIO	59.3 92.7 87.2 .0 .0 .0 MS/COMMENTS THE UTILITY R THROUGH JUNE LEED LINE PR 983.	59.3 92.7 87.2 .0 EPORTED THICK 1983. OBLEMS WERE	52.4 81.5 67.2 .0 .0 KENER PROBLEM	NCED DU	RING '	672 744 720 744 720 E PERIO	594 654 555 184 151 OD OF J	352 606 484 0 0	50.0 50.0 50.0 50.0
2/83 3/63 3/63 4/83 5/83 6/83	SYSTEM SYSTEM SYSTEM SYSTEM SYSTEM	56.3 93.5 86.8 .0 .0 .0 BLEMS/SOLUTIO	59.3 92.7 87.2 .0 .0 .NS/COMMENTS THE UTILITY R THROUGH JUNE LEED LINE PR 983. TUMP FAILURES	59.3 92.7 87.2 .0 EPORTED THICK 1983. OBLEMS WERE	52.4 81.5 67.2 .0 .0 KENER PROBLEM ALSO EXPERIEN ED CAUSING OL	NCED DU	RING '	672 744 720 744 720 E PERIO	594 654 555 184 151 OD OF J. RST SIX	352 606 484 0 0 ANUARY MONTHS	50.0 50.0 50.0 50.0
2/83 3/83 3/83 4/83 5/83 6/83	SYSTEM SYSTEM SYSTEM SYSTEM ** PRO	56.3 93.5 86.8 .0 .0 BLEMS/SOLUTIO	59.3 92.7 87.2 .0 .0 .0 MS/COMMENTS HE UTILITY R HROUGH JUNE LEED LINE PR 983. TUMP FAILURES ANUARY THROU	59.3 92.7 87.2 .0 EPORTED THICE 1983. OBLEMS WERE WERE REPORT GH JUNE 1983	52.4 81.5 67.2 .0 .0 KENER PROBLEM ALSO EXPERIEN ED CAUSING OU . 63.6	NCED DU	RING '	672 744 720 744 720 THE FIR	594 654 555 184 151 DD OF J. RST SIX THE PER.	352 606 484 0 0 ANUARY MONTHS	50.0 50.0 50.0 50.0 50.0

10/83 SYSTEM 77.6 72.9 72.9 48.4 744 494 360

OF 1983.

THE THIRD QUARTER.

REPAIRS ON THE ABSORBER VENT SYSTEM WERE MADE DURING THE THIRD QUARTER

THE NEED TO ISOLATE THE SERVICE WATER SYSTEM RESULTED IN DOWN TIME DURING

LOUISVILLE GAS & ELECTRIC: MILL CREEK 2 (CONT.)

				PERFORMAN							
PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION				BOILER HOURS		CAP. FACTOR
				·							
11/83	SYSTEM	70.4	58.9	58. 9	45.1			720	552	325	
12/83	SYSTEM	58.3	47.7	47.7	39.1			744	610	291	
	** PROB	BLEMS/SOLUTION	NS/COMMENTS								
		N	MAJOR FGD-	RELATED PROBL	EMS WERE REF	ORTED	FOR T	HE FOUT	TH QUAR	RTER OF	1983.
1/84	SYSTEM							744			
2/84	SYSTEM							696			
3/84	SYSTEM							744			
4/84	SYSTEM							720			
5/84	SYSTEM							744			
6/84	SYSTEM							720			
7/84	SYSTEM							744			
8/84	SYSTEM							744			
9/84	SYSTEM							720			

^{**} PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE FIRST THREE QUARTERS OF 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

LOUISVILLE GAS & ELECTRIC COMPANY NAME PLANT NAME MILL CREEK UNIT NUMBER 3 LOUISVILLE CITY STATE KENTUCKY REGULATORY CLASSIFICATION 43. 516. PARTICULATE EMISSION LIMITATION - NG/J (.100 LB/MMBTU) (1.200 LB/MMBTU) (.700 LB/MMBTU) SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J 301. NET PLANT GENERATING CAPACITY - MW 1084 GROSS UNIT GENERATING CAPACITY - MW 427 NET UNIT GENERATING CAPACITY W/FGD - MW 420 NET UNIT GENERATING CAPACITY WO/FGD - MW 495 EQUIVALENT SCRUBBED CAPACITY - MW 427 ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER BABCOCK & WILCOX BOILER TYFE PULVERIZED COAL BOILER SERVICE LOAD BASE 755.04 148.9 183. CONCRETE (1600000 ACFM) (300 F) (600 FT) DESIGN BOILER FLUE GAS FLOW - CU.M/S BOILER FLUE GAS TEMPERATURE - C STACK HEIGHT - M STACK SHELL STACK TOP DIAMETER - M 6.4 (21.0 FT) ** FUEL DATA FUEL TYPE COAL FUEL GRADE BITUMINOUS 26284. AVERAGE HEAT CONTENT - J/G (11300 BTU/LB) RANGE HEAT CONTENT - BTU/LB 11000-12000 AVERAGE ASH CONTENT - % 15.00 RANGE ASH CONTENT - % 13.0-16.0 AVERAGE MOISTURE CONTENT - % 10.00 9.0-15.0 RANGE MOISTURE CONTENT + % 3.87 AVERAGE SULFUR CONTENT - % RANGE SULFUR CONTENT - % 3.5-4.0 .04 AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - % .03-.06 *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER Ω NONE TYPE ** FABRIC FILTER Ω NUMBER NONE TYPE ** ESP NUMBER NUMBER OF SPARES COLD SIDE TYPE 377.5 (800000 ACFM) 148.9 (300 F) SUPPLIER INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS TEMPERATURE - C 99.5 PARTICLE REMOVAL EFFICENCY + % ** PARTICLE SCRUBBER Λ NUMBER NONE GENERIC TYPE SPECIFIC TYPE N/A N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL LINER GENERIC MATERIAL N/A N/A

LINER SPECIFIC MATERIAL

*** FGD SYSTEM

```
** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                              THROWAWAY PRODUCT
                                              WET SCRUBBING
   SO2 REMOVAL MODE
                                              LIME
   PROCESS TYPE
   SYSTEM SUPPLIER
                                              AMERICAN AIR FILTER
                                              FLUOR POWER SERVICES
   A-E FIRM
                                              FULL SCALE
   DEVELOPMENT LEVEL
                                              NEM
   NEW/RETROFIT
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.00
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                85.00
    CURRENT STATUS
   COMMERCIAL START-UP
                                               3/79
                                               8/78
    INITIAL START-UP
   CONTRACT AWARDED
                                              11/75
** DESIGN AND OPERATING PARAMETERS
                                                4.00
    DESIGN COAL SULFER CONTENT - %
                                            27912.0
    DESIGN COAL HEAT CONTENT - J/G
                                                            ( 12000 BTU/LB)
    DESIGN COAL ASH CONTENT - X
                                               16.00
    DESIGN MOISTURE CONTENT - X
                                                15.00
    DESIGN CHLORIDE CONTENT - X
                                                   . 06
    OPER. & MAINT, REQUIREMENT - MANHR/DAY
                                               120.0
** QUENCHER/PRESATURATOR
    NUMBER
    TYPE
                                              VENTURI
    SUPPLIER
                                              AMERICAN AIR FILTER
                                               188.76 ( 400000 ACFM)
148.9 ( 300 F)
    INLET GAS FLOW - CU. M/S
    INLET GAS TEMPERATURE - C
                                              .5
126.
.7
                                                            ( 2.0 IN-H20)
    PRESSURE DROP - KPA
    LIQUID RECIRCULATION RATE - LITERS/S
                                                            ( 2000 GPM)
                                                            ( 5.0 GAL/1000 ACFM)
    L/G RATIO - L/CU. M
                                             CARBON STEEL
    CONSTRUCTION MATERIAL GENERIC TYPE
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                             AISI 1110
** ABSORBER
    NUMBER
                                               4
    NUMBER OF SPARES
                                               0
    GENERIC TYPE
                                              PACKED TOWER
    SPECIFIC TYPE
                                              ENTRAINED PACKING
    TRADE NAME/COMMON TYPE
                                              MOBILE BED CONTACTOR
    SUPPLIER
                                              AMERICAN AIR FILTER
    DIMENSIONS - FT
                                              16.0 X 20.0
    SHELL GENERIC MATERIAL
                                              CARBON STEEL
    SHELL SPECIFIC MATERIAL
                                              AISI 1110
    SHELL MATERIAL TRADE NAME/COMMON TYPE N/A
    LINER GENERIC MATERIAL
                                              THORGANIC
    LINER SPECIFIC MATERIAL
                                              HYDRAULICALLY-BONDED MORTAR
    LINER MATERIAL TRADE NAME/COMMON TYPE
GAS CONTACTING DEVICE TYPE
                                              PRE-KRETE G-8
                                              POLYURETHANE BALLS
    NUMBER OF CONTACTING ZONES
                                               1
    LIQUID RECIRCULATION RATE - LITER/S
                                               1285.
                                                            (20400 GPM)
                                               7.4
    L/G RATIO - L/CU.M
                                                            ( 55.0 GAL/1000 ACF)
    GAS-SIDE PRESSURE DROP - KPA
                                                 1.5
                                                            ( 6.0 IN-H2O)
                                                            ( 10.0 FT/S)
( 370900 ACFM)
    SUPERFICAL GAS VELOCITY - M/SEC
                                                  3.0
                                              175.03
    INLET GAS FLOW - CU. M/S
    INLET GAS TEMPERATURE - C
                                                            ( 300 F)
                                               148.9
    SO2 REMOVAL EFFICIENCY %
                                                 85.7
** MIST ELIMINATOR
    PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                              PRIMARY COLLECTOR
    NUMBER PER SYSTEM
                                               8
    NUMBER OF SPARES PER SYSTEM
                                               0
    NUMBER PER MODULE
                                               2
    GENERIC TYPE
                                              IMPINGEMENT
    SPECIFIC TYPE
                                              BAFFLE
    TRADE NAME/COMMON TYPE
                                              CLOSED VANE
    MANUFACTURER
                                              ATLANTIC BRIDGE
```

```
CONFIGURATION
                                              HORIZONTAL
   NUMBER OF STAGES
                                                  1
   NUMBER OF PASSES PER STAGE
                                                  3
   FREEBOARD DISTANCE - M
                                                  2.13
                                                             ( 7.0 FT)
   DISTANCE BETWEEN STAGES - CM
                                                  7.62
                                                             ( 3.0 IN)
   DISTANCE BETWEEN VANES - CM
                                                  2.5
                                                             ( 1.00 IN)
   PRESSURE DROP - KPA
                                                  . 2
                                                             ( 1.0 IN-H20)
   SUPERFICAL GAS VELOCITY - M/S
                                                  4.6
                                                             ( 15.0 FT/S)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              STAINLESS STEEL
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              AUSTENTITIC
   WASH WATER SOURCE
                                              FRESH
   WASH FREQUENCY
                                              10% OF THE AREA WASHED EACH 1/2 MINUTE
   WASH RATE - L/S
                                                  2.5
                                                            ( 40 GAL/MIN)
** REHEATER
   NUMBER
                                               4
   NUMBER OF SPARES
                                               0
   NUMBER PER MODULE
                                               1
   GENERIC TYPE
                                              IN-LINE
   SPECIFIC TYPE
                                              STEAM
   TRADE NAME/COMMON TYPE
                                              BARE TUBE
   LOCATION
                                              TOP OF ABSORBER
   TEMPERATURE INCREASE - C
                                               27.8 (
                                                                50 F)
                                                             ( 130 F)
   INLET FLUE GAS TEMPERATURE - C
                                                 54.4
                                                             ( 180 F)
   OUTLET FLUE GAS TEMPERATURE - C
                                                 82.2
   CONSTRUCTION MATERIAL GENERIC TYPE
                                             CARBON STEEL
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                             AISI 1110
   NUMBER
                                               2
   NUMBER OF SPARES
                                               0
                                              CENTRIFUGAL
   DESTEN
   SUPPLIER
                                              AMERICAN STANDARD
   FUNCTION
                                              UNIT
   APPLICATION
                                              FORCED DRAFT
   SERVICE
                                              DRY
   FLUE GAS FLOW RATE - CU.M/S
                                               377.52
                                                             ( 800000 ACFM)
   FLUE GAS TEMPERATURE - C
                                                148.9
                                                             ( 300 F)
   PRESSURE DROP - KPA
                                                 12.9
                                                             (42.3 IN-H20)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              CARBON STEEL
** DAMPERS
   NUMBER
                                               2
                                              SHUT-OFF
   FUNCTION
   GENERIC TYPE
                                              GUILLOTINE
   SPECIFIC TYPE
                                              TOP-ENTRY GUILLOTINE
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              STAINLESS STEEL
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              AUSTENTITC
   LINER GENERIC MATERIAL TYPE
                                              NONE
   LINER SPECIFIC MATERIAL TYPE
                                              N/A
** DAMPERS
                                               2
   NUMBER
   FUNCTION
                                              SHUT-OFF
                                              GUILLOTINE
   GENERIC TYPE
                                              TOP-ENTRY GUILLOTINE
   SPECIFIC TYPE
                                              STAINLESS STEEL
   CONSTRUCTION MATERIAL GENERIC TYPE
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              AUSTENITIC
   LINER GENERIC MATERIAL TYPE
                                              NONE
   LINER SPECIFIC MATERIAL TYPE
                                              N/A
** DAMPERS
                                               2
   NUMBER
                                              SHUT-OFF
   FUNCTION
                                              GUILLOTINE
   GENERIC TYPE
   SPECIFIC TYPE
                                              TOP-ENTRY GUILLOTINE
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              STAINLESS STEEL
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              AUSTENITIC
                                              NONE
   LINER GENERIC MATERIAL TYPE
   LINER SPECIFIC MATERIAL TYPE
                                              N/A
```

**	DUCTWORK	ADCOURED THEFT
	LOCATION	ABSORBER INLET
	SHELL GENERIC MATERIAL TYPE	CARBON STEEL ATSI 1110
	SHELL SPECIFIC MATERIAL TYPE	NONE
	LINER GENERIC MATERIAL TYPE	N/A
	LINER SPECIFIC MATERIAL TYPE	N/ A
¥¥	DUCTHORK	ABSORBER OUTLET
	LOCATION SHELL GENERIC MATERIAL TYPE	CARBON STEEL
	SHELL SPECIFIC MATERIAL TYPE	AISI 1110
	LINER GENERIC MATERIAL TYPE	INORGANIC
	LINER SPECIFIC MATERIAL TYPE	HYDRAULICALLY-BONDED MORTAR
**	DUCTWORK	
	LOCATION	DOWNSTREAM OF REHEATER
	SHELL GENERIC MATERIAL TYPE	CARBON STEEL
	SHELL SPECIFIC MATERIAL TYPE	AISI 1110
	LINER GENERIC MATERIAL TYPE	ORGANIC
	LINER SPECIFIC MATERIAL TYPE	HYDRAULICALLY-BONDED MORTAR
××	DUCTWORK	DVD466
	LOCATION	BYPASS CARBON STEEL
	SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE	AISI 1110
	LINER GENERIC MATERIAL TYPE	INORGANIC
	LINER SPECIFIC MATERIAL TYPE	FOAM GLASS BLOCKS
	LINER SPECIFIC MATERIAL TIPE	TOAL GEAGG BEGGRO
**	REAGENT PREPARATION EQUIPMENT	
	FUNCTION	WET BALL MILL
	DEVICE TYPE	COMPARTMENTED
	DEVICE TYPE NUMBER	TUBE MILL
	NUMBER OF SPARES	1
	PRODUCT QUALITY - % SOLIDS	25.0
		23.0
**	TANKS SERVICE	NUMBER
	CARBIDE LIME SLURRY	2
	ADDITIVE SLURRY DAY	ī
	REACTION	4
	THICKENER	1
××	PUMPS	
	SERVICE	NUMBER
	ADDITIVE SLURRY TRANSFER	7
	RECYCLE	10
	ABSORBER BLEED	6
	THICKENER UNDERFLOW	2
××	SOLIDS CONCENTRATING/DEWATERING	
	DEVICE	THICKENER
	NUMBER	1
	NUMBER OF SPARES	0
	DIMENSIONS - FT	125.0 X 10.0
	SHELL GENERIC MATERIAL TYPE	CARBON STEEL
	SHELL SPECIFIC MATERIAL TYPE	AISI 1110
	LINER GENERIC MATERIAL TYPE	NONE
	LINER SPECIFIC MATERIAL TYPE FEED STREAM SOUPCE	N/A
		ABSORBER BLEED
	FEED STREAM CHARACTERISTICS OUTLET STREAM CHARACTERISTICS	10% SOLIDS
	OUTLET STREAM DISPOSITION	20% SOLIDS
		VACUUM FILTER
**	SOLIDS CONCENTRATING/DEWATERING DEVICE	VACUEDA ETITO
	20,400	VACUUM FILTER

5 1

NUMBER

NUMBER OF SPARES

FEED STREAM SOURCE THICKENER UNDERFLOW FEED STREAM CHARACTERISTICS 20% SOLIDS OUTLET STREAM CHARACTERISTICS 45% SOLIDS OUTLET STREAM DISPOSITION PUG MILL

*** SALEABLE BYPRODUCTS

NATURE NONE

*** SLUDGE

** TREATMENT
METHOD
DEVICE

DEVICE PUG MILL
PROFRIETARY PROCESS CONVERSION SYSTEMS [POZ-0-TEC]

FIXATION

INLET QUALITY - % 45.0

** DISPOSAL

NATURE FINAL
TYPE LANDFILL
LOCATION ON-SITE
SITE TRANSPORTATION METHOD TRUCK
SITE TREATMENT CLAY LINING
SITE SERVICE LIFE - YRS 10

** PROCESS CONTROL AND INSTRUMENTATION

PROCESS STREAM SLURRY RECYCLE
CHEMICAL PARAMETERS PH
MONITOR TYPE UNILOC
MONITOR LOCATION IN REACTION TANK

PROCESS CHEMISTRY MODE FEEDBACK

PROCESS CHEMISIKI HODE FEEDBA

** WATER BALANCE

WATER LOOP TYPE OPEN/CLOSED

MAKEUP WATER ADDITION - LITERS/S 9.4 (150 GPM)

** CHEMICALS AND CONSUMPTION

FUNCTION ABSORBENT
NAME CARBIDE LIME
PRINCIPAL CONSTITUENT 90% CAOH2
SOURCE/SUPPLIER AIRCO
POINT OF ADDITION RECYCLE TANK

** FGD SPARE CAPACITY INDICES

.0 ABSCRBER % .0 MIST ELIMINATOR - % REHEATER - % .0 .0 FAN Z BALL MILL - % .0 EFFLUENT HOLD TANK - % .0 RECIRCULATION PUMP % 25.0 THICKENER % .0 VACUUM FILTER - % .0

** FGD SPARE COMPONENT INDICES

.0 ABSORBER .0 MIST ELIMINATOR .0 REHEATER .0 FAN .0 BALL MILL .0 EFFLUENT HOLD TANK 1.0 RECIRCULATION PUMP .0 THICKENER .0 VACUUM FILTER

							PART.	HOURS	HOURS	HOURS	FACTOR
	OVETEN										
	SYSTEM							744			
	** PROBLE	1S/SOLUTI	NS/COMMENTS								
			INITIAL FGD O		GAN ON AUGUS	ST 13,	1978.	OPERA	ATIONAL	HOURS	WERE
9/78	SYSTEM	81.0	80.7	80.0	80.0			720	714	576	52.0
	** PROBLEM	HS/SOLUTI	ONS/COMMENTS								
			FRP PIPING PR	OBLEMS WERE	ENCOUNTERED.						
			SOME BEARING DURING SEPTEM		LATED PUMP F	ROBLE	1S WER	E ALSO	ENCOUNT	TERED	
10/78	SYSTEM	86.0	85.5	85.0	81.6			744	710	607	54.0
11/78	SYSTEM	93.0	85.2	85.0	41.5			720	351	299	40.0
	** PROBLE	1S/SOLUTI	ONS/COMMENTS								
			THE UNIT WAS RESTART IS PR				OR SCH	EDULED	INSPEC	TION.	
12/78	SYSTEM				.0			744	0	0	.0
1/79	SYSTEM				.0			744	0	0	.0
	** PROBLE	MS/SOLUTI	ONS/COMMENTS								
			THE UNIT DID N	OT OPERATE D	URING DECEME	BER OR	JANUA	RY.			
2/79	ŞYSTEM	26.0	18.0	18.0	17.4			672	651	117	52.0
3/79	SYSTEM	62.0	53.1	53.0	52.4			744	735	390	51.0
	** PROBLE	MS/SOLUTI	ONS/COMMENTS								
			COMPLIANCE TES	TING WAS PER	FORMED DURIN	NG MAR	CH AND	THE U	CAW TIN	DECLAS	RED
4/79	SYSTEM	75.0	63.6	63.0	44.4			720	503	320	40.0
	** PROBLE	MS/SOLUTI	ONS/COMMENTS								
			THE ONLY PROBL	EMS REPORTED	WERE WITH	DAMPER	S AND	PUMP F	AILURES	•	
5/79	SYSTEM	100.0	97.8	97.0	64.7			744	492	481	38.0
6/79	SYSTEM	56.0	51.9	51.0	47.9			720	665	345	48.0
	** PROBLE	MS/SOLUTI	ONS/COMMENTS							714 576 ENCOUNTERED 710 607 351 299 INSPECTION. 0 0 0 0 651 117 735 390 IT WAS DECLAR 503 320 ILURES. 492 481 665 345	
			THE UTILITY RE		NO UNUSUAL (OPERAT	ING PR	OBLEMS	WERE E	исоинт	ERED
7/79	SYSTEM	63.0	59.9	59.0	55.2			744	686	411	53.0
8/79	SYSTEM	76.0	68.0	68.0	50.3			744	550	374	47.0

PERIOD	MODULE		TY OPERABILITY	RELIABILITY	UTILIZATION		VAL PER			
	** PROB	LEMS/SOLUT	IONS/COMMENTS							
			IN JULY AND AN							WILL
9/79	SYSTEM	91.0	90.6	91.0	83.9		72	20 667	604	50.0
.0/79	SYSTEM	83.0	82.0	82.0	76.1		79	44 690	566	44.0
	** PROB	LEMS/SOLUT	IONS/COMMENTS							
			AT THE END OF SCHEDULED TO I						IL AND	IS
11/79	SYSTEM				.0		7:	20 0	0	.0
12/79	SYSTEM				.0		74	44 0	0	.0
1/80	SYSTEM				.0		79	44 0	0	.0
	** PROB	LEMS/SOLUT	IONS/COMMENTS							
			DURING THE OVE		AL SCRUBBER M	1AINTENA	NCE WAS I	OONE BUT	LAM ON	OR .
2/80	SYSTEM	37.0	36.1	36.0	26.6		6	96 512	185	39.0
	** PROE	LEMS/SOLUT	IONS/COMMENTS							
			THE UNIT CAME WORK WAS COMP	•	E ON FEBRUARY	Y 10 AFT	ER THE TO	JRBINE OV	'ERHAUL	
3/80	SYSTEM	37.0	36.9	37.0	30.6		74	44 618	228	46.0
	** PROE	LEMS/SOLUT	IONS/COMMENTS							
			PROBLEMS ENCO OPERATION INC REHEATER FLAN	LUDED FROZEN						E
			THE UTILITY I	S IN THE PRO	CESS OF REPLA	ACING TH	E REHEAT	ER TUBES.		
4/80	SYSTEM	42.9	42.5	42.5	42.2		7:	20 715	304	53.0
	** PROE	SLEMS/SOLUT	IONS/COMMENTS							
			THE REHEATER	TUBE REPLACE	MENT CONTINUE	ED INTO	APRIL.			
			THE OTHER OUT			ING APRI	L WAS CA	USED BY A	L BLOWN	
5/80	SYSTEM	67.5	51.4	51.4	34.4		7	44 498	256	47.0
	** PROB	LEMS/SOLUT	IONS/COMMENTS							
			DURING MAY TH	E PLASTIC MI EL. THIS KE	ST ELIMINATOR PT THE SYSTEM	R COMPON M OFF LI	NENTS WER	E REPLACE PPROXIMAT	ED WITH	DAYS.

6/80 SYSTEM 88.2 .0 .0 .0

REHEATER TUBE LEAKS WERE ALSO ENCOUNTERED IN MAY.

720 85 0 14.0

LOUISVILLE GAS & ELECTRIC: MILL CREEK 3 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

IN LATE MAY THE TURBINE LOST TWO BLADES CAUSING THE SYSTEM TO SHUTDOWN UNTIL THE LATTER PART OF JUNE. DURING THE OUTAGE THE UTILITY DECIDED TO REPLACE THE LIME STORAGE TANK LINES WITH LARGER ONES TO SERVICE THE NEW UNITS. THE WORK WAS NOT COMPLETED WHEN THE BOILER WAS RETURNED TO SERVICE; THUS, THE FGD UNIT DID NOT OPERATE DURING THE MONTH.

7/80 SYSTEM 92.0 91.3 91.3 83.9 744 684 625 52.0

** PROBLEMS/SOLUTIONS/COMMENTS

RECYCLE PUMP FAILURES CAUSED THE FGD SYSTEM TO SHUTDOWN FOR PART OF JULY.

8/80	SYSTEM	58.7	81.7	81.7	58.7	744	535	437	60.0
9/80	SYSTEM	57.2	60.4	60.4	57.2	720	682	412	60.0

** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE AUGUST THROUGH SEPTEMBER PERIOD THE PUMP HOUSE WAS FLOODED DUE TO THE FAILURE OF THE BLEED PUMP FRP PIPE LINE. BECAUSE OF THIS FAILURE, 23 PUMPS AND 23 PUMP MOTORS WERE DAMAGED.

10/80 SYSTEM 100.0 97.1 97.1 96.9 744 742 721 99.7

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE MONTH OF OCTOBER.

11/80 SYSTEM 57.1 49.4 49.4 41.9 720 611 302 60.0

** PROBLEMS/SOLUTIONS/COMMENTS

DURING NOVEMBER OPERATION OF THE FGD SYSTEM WAS LOW DUE TO PUMP DAMAGES WHICH RESULTED FROM THE PUMP HOUSE FLOODING IN AUGUST.

12/80 SYSTEM 100.0 100.0 100.0 61.1 744 455 455 60.0

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE MONTH OF DECEMBER.

1/81	SYSTEM	. 0	. 0	.0	.0	744	521	0	40.0
2/81	SYSTEM	.0	.0	.0	.0	672	593	0	50.0
3/81	SYSTEM	1.0	1.0	1.0	1.0	744	675	8	50.0

** FROBLEMS/SOLUTIONS/COMMENTS

DURING THE FIRST QUARTER 1981 MAJOR CORROSION DAMAGE CAUSED FAILURE OF THE PRECRETE-G.

FROZEN LINES ENCOUNTERED DURING THE PERIOD ACCOUNTED FOR SOME OUTAGE TIME.

REPAIRS TO THE MIST ELIMINATOR SHELL CAUSED ADDITIONAL OUTAGE TIME.

DURING MARCH STRIKING WORKERS ADDED TO THE OUTAGE TIME OF THE SYSTEM.

4/81 SYSTEM 32.9 33.2 33.2 32.9 720 714 237 45.0

720 502 64 50.0

ERIOD	MODULE	AVAILABILI	TY OPERABILITY		UTILIZATION	502	PART.	HOURS	HOURS	HOURS	FACTOR
	** PROE	LEMS/SOLUT	IONS/COMMENTS								
			DURING THE MOR		THE UTILITY	REPOR	TED HA	VING PF	ROBLEMS	WITH F	FROZEN
5/81	SYSTEM	33.7	37.9	37.9	33.7			744	662	251	55.0
	** PROE	LEMS/SOLUT	IONS/COMMENTS								
			DURING THE MOI		HE UTILITY RE	PORTE	IVAH C	NG PROI	BLEMS W	ITH	
6/81	SYSTEM	34.6	34.6	34.6	34.6			720	719	249	
	** PROE	BLEMS/SOLUT	IONS/COMMENTS								
			DURING THE MOI	TH OF JUNE	THE UTILITY F	REPORT	ED HAV	ING MOI	OULE CO	ROSIO	4
7/81	SYSTEM	63.4	73.6	73.6	63.4			744	641	472	60.0
8/81	SYSTEM	89.2	91.8	91.8	88.3			744	716	657	65.0
9/81	SYSTEM	80.8	80.8	80.8	80.8			720	720	582	65.0
	** PROE	BLEMS/SOLUT	IONS/COMMENTS								
			MIST ELIMINAT	OR MODULE FA	ILURES WERE E	ENCOUN	TERED	DURING	THE TH	IRD QU	ARTER
10/81	SYSTEM	41.4	89.7	89.7	41.4			744	332	298	50.0
11/81	SYSTEM	32.4	37.4	37.4	32.4			720	623	233	50. 0
12/81	SYSTEM	41.4	42.7	42.7	41.4			744	721	308	50.0
	** PROS	BLEMS/SOLUT	IONS/COMMENTS								
			DURING THE FO	URTH QUARTER	PUMP FAILURE	ES WER	E ENCO	UNTERE	D.		
			PROBLEMS DURI	NG THE PERIO	D WERE ALSO I	EXPERI	ENCED	WITH T	HE THIC	KENER	ДИA
1/82	SYSTEM	.0	.0		.0			744	743	0	50.0
2/82	SYSTEM	.0	.0		.0			672	612	0	50.0
3/82	SYSTEM	.0	.0		.0			744	202	0	50.0
	** PRO	BLEMS/SOLUT	IONS/COMMENTS								
			DURING THE FI			SYSTE	M WAS	OFF-LI	NE TO R	EBUILD	
4/82	SYSTEM	.0	.0	.0	.0			720	704	0	50.0
5/82	SYSTEM	.0	.0	.0	.0			744	665	0	50.0

6/82 SYSTEM 8.9 12.7 12.7 8.9

LOUISVILLE GAS & ELECTRIC: MILL CREEK 3 (CONT.)

PERIOD			Y OPERABILITY	PERFORMAN RELIABILITY	UTILIZATION	% REMOVAL SO2 PART	PER	BOILER	FGD	CAP.
	** PROE	SLEMS/SOLUTI	ONS/COMMENTS							
			DURING THE SE	COND QUARTER,	THE MIST EL	IMINATOR S	HELL ON	ALL MO	DULES I	4AS
7/82	SYSTEM	36.4	36.5	36.5	36.4		744	742	271	50.0
8/82	SYSTEM	60.5	59.8	59.8	58.3		744	726	434	50.0
9/82	SYSTEM	15.3	43.7	43.7	15.3		720	252	110	50.0
	** PROB	BLEMS/SOLUTI	ONS/COMMENTS							
				EPORTED THAT Y, AUGUST AND			E EXPER	IENCED I	DURING	THE
10/82	SYSTEM	71.5	73.4	73.4	59.7		744	605	444	50.0
11/82	SYSTEM	74.0	60.6	60.6	30.1		720	358	217	50.0
12/82	SYSTEM	.0	.0	.0	.0		744	550	0	50.0
	** PROS	BLEMS/SOLUTI	ONS/COMMENTS							
				EPORTED THAT Y THROUGH DEC		ATORS WERE	BEING R	EBUILT	DURING	THE
			REHEAT TUBES	WERE ALSO REB	UILT/REPLACE	D DURING T	HIS PER	IOD.		
1/83	SYSTEM	.0	.0	.0	.0			42	0	50.0
2/83	SYSTEM	9.4	71.6	71.6	9.4		672	88	63	50.0
3/83	SYSTEM	25.0	41.0	41.0	25.0		744	454	186	50.0
4/83	SYSTEM	.0	.0	.0	.0		720	416	0	50.0
5/83	SYSTEM	57.0	72.5		56.5		744	579	420	50.0
6/83	SYSTEM	30.0	43.1	43.1	30.0		720	501	216	50.0
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS							
				EPORTED PROBL		JGGING IN T	HE REHE	ATER DU	RING T	НE
				E REHEAT TUBE		OURING THE	FIRST S	IX MONT	HS OF	1983
7/83	SYSTEM	28.1	28.2	28.2	28.1		744	742	209	50.0
8/83	SYSTEM	2.7	2.7	2.7	2.7		744	737	20	50.0
9/83	SYSTEM	.0	.0	.0	. 0		720	659	0	50.0
	** PRO	BLEMS/SOLUTI	ONS/COMMENTS							
			LEAKS IN THE	STACK REHEAT	SYSTEM WERE	REPAIRED D	URING T	HE THIR	D QUAR	TER OF
10/83	SYSTEM	13.8	14.7	14.7	13.6		744	685	101	

.0

720 0 0

11/83 SYSTEM 56.7

PERFORMANCE DATA											
PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% RE	MOVAL	PER	BOILER	FGD	CAP.
						502	PART.	HOURS	HOURS	HOURS	FACTOR
12/83	SYSTEM	25.9	8.6	8.6	6.7			744	583	25	
	** DOOR! FMS /SOLLITTONS /COMMENTS										

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE REPORTED FOR THE FOURTH QUARTER OF 1983.

1/84	SYSTEM	744
2/84	SYSTEM	696
3/84	SYSTEM	744
4/84	SYSTEM	720
5/84	SYSTEM	744
6/84	SYSTEM	720
7/84	SYSTEM	744
8/84	SYSTEM	744
9/84	SYSTEM	720

^{**} PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE FIRST THREE QUARTERS OF 1984.

SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

LOUISVILLE GAS & ELECTRIC COMPANY NAME MILL CREEK PLANT NAME UNIT NUMBER LOUISVILLE CITY STATE KENTUCKY REGULATORY CLASSIFICATION PARTICULATE EMISSION LIMITATION - NG/J 43. (.100 LB/MMBTU)
S02 EMISSION LIMITATION - NG/J 516. (1.200 LB/MMBTU)
NOX EMISSION LIMITATION NG/J 301. (.700 LB/MMBTU)
NET PLANT GENERATING CAPACITY - MW 495 GROSS UNIT GENERATING CAPACITY - MW
NET UNIT GENERATING CAPACITY W/FGD - MW
NET UNIT GENERATING CAPACITY WO/FGD - MW 495 495 495 FQUIVALENT SCRUBBED CAPACITY - MW 495 ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER BABCOCK & WILCOX BOILER TYPE PULVERIZED COAL DESIGN BOILER FLUE GAS FLOW - CU.M/S
BOILER FLUE GAS TEMPERATURE - C
STACK HEIGHT - M BASE BOILER SERVICE LOAD 755.04 (1600000 ACFM)
148.9 (300 F)
183. (600 FT)
CONCRETE STACK SHELL ***** STACK TOP DIAMETER - M (**** FT) ** FUEL DATA FUEL TYPE COAL BITUMINOUS FUEL GRADE AVERAGE HEAT CONTENT J/G 26749. (11500 BTU/LB) RANGE HEAT CONTENT - BTU/LB 11000-12000 15.00 AVERAGE ASH CONTENT - % 15.00 13.0-16.0 10.00 3.5-4.0 3.75 RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - %
RANGE MOISTURE CONTENT - %
AVERAGE SULFUR CONTENT - %
RANGE SULFUR CONTENT - % RANGE SULFUR CONTENT - %
AVERAGE CHLORIDE CONTENT - % ****** .08 .03-.06 .08 *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER n TYPE NONE ** FABRIC FILTER NUMBER Ω TYPE NONE ** FSP NUMBER 2 NUMBER OF SPARES O TYPE COLD SIDE SUPPLIER AMERICAN AIR FILTER INLET FLUE GAS CAPACITY - CU.M/S
INLET FLUE GAS TEMPERATURE - C 377.5 (800000 ACFM) 148.9 (300 F) PARTICLE REMOVAL EFFICENCY - % 99.5 ** PARTICLE SCRUBBER NUMBER 0 GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL N/A LINER GENERIC MATEPIAL N/A LINER SPECIFIC MATERIAL N/A

INUISVILLE GAS & ELECTRIC: MILL CREEK 4 (CONT.)

*** FGD SYSTEM

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** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                              THROWAWAY PRODUCT
   SO2 REMOVAL MODE
                                              WET SCRUBBING
   PROCESS TYPE
                                              LIME
   SYSTEM SUPPLIER
                                              AMERICAN AIR FILTER
                                              FLUOR POWER SERVICES
   A-E FIRM
   DEVELOPMENT LEVEL
                                              FULL SCALE
   NEW/RETROFIT
                                              NFW
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - X
                                                85.00
   CURRENT STATUS
                                               7
   COMMERCIAL START-UP
                                              10/82
   INITIAL START-UP
                                               7/82
   CONTRACT AWARDED
                                               2/76
** DESIGN AND OPERATING PARAMETERS
   DESIGN COAL SULFER CONTENT - %
                                                  4.00
   DESIGN COAL HEAT CONTENT - J/G
                                              27912.0
                                                             ( 12000 BTU/LB)
   DESIGN COAL ASH CONTENT - %
                                                16.00
   DESIGN MOISTURE CONTENT - %
                                                 15.00
   DESIGN CHLORIDE CONTENT - X
                                                   .06
** QUENCHER/PRESATURATOR
   NUMBER
                                              VENTURI
   TYPE
   SUPPLIER
                                              AMERICAN AIR FILTER
   INLET GAS FLOW - CU. M/S
                                               188.76 ( 400000 ACFM)
                                                             ( 300 F)
( 5.0 GAL/1000 ACFM)
   INLET GAS TEMPERATURE - C
                                                148.9
   L/G RATIO - L/CU. M
                                                  . 7
   CONSTRUCTION MATERIAL GENERIC TYPE
                                            CARBON STEEL
                                             AISI 1110
   CONSTRUCTION MATERIAL SPECIFIC TYPE
** ABSORBER
   NUMBER
   NUMBER OF SPARES
                                               Λ
   GENERIC TYPE
                                              PACKED TOWER
                                              ENTRAINED PACKING
   SPECIFIC TYPE
   TRADE NAME/COMMON TYPE
                                              MOBILE BED CONTACTOR
   SUPPLIER
                                              AMERICAN AIR FILTER
   DIMENSIONS - FT
                                              16.0 X 20.0
                                              CARBON STEEL
   SHELL GENERIC MATERIAL
   SHELL SPECIFIC MATERIAL
                                              AISI 1110
   SHELL MATERIAL TRADE NAME/COMMON TYPE
                                              N/A
                                              INORGANIC
   LINER GENERIC MATERIAL
   LINER SPECIFIC MATERIAL
                                              HYDRAULICALLY-BONDED MORTAR
   LINER MATERIAL TRADE NAME/COMMON TYPE
                                              PRE-KRETE G-8
   GAS CONTACTING DEVICE TYPE
                                              POLYURETHANE BALLS
                                                           (20400 GPM)
   LIQUID RECIRCULATION RATE - LITER/S
                                               1285.
   SUPERFICAL GAS VELOCITY - M/SEC
                                                 3.0
                                                             ( 10.0 FT/S)
   SO2 REMOVAL EFFICIENCY - %
                                                 85.0
** MIST ELIMINATOR
                                              PRIMARY COLLECTOR
   PRE-MIST ELIMINATOR/MIST ELIMINATOR
   NUMBER PER SYSTEM
                                              8
   NUMBER OF SPARES PER SYSTEM
                                               0
   NUMBER FER MODULE
                                               2
                                              IMPINGEMENT
   GENERIC TYPE
   SPECIFIC TYPE
                                              BAFFLE
                                              CLOSED VANE
   TRADE NAME/COMMON TYPE
   MANUFACTURER
                                              ATLANTIC BRIDGE
   CONFIGURATION
                                              HORIZONTAL
   NUMBER OF PASSES PER STAGE
                                                  3
                                                  2.13
                                                             ( 7.0 FT)
   FREEBOARD DISTANCE M
                                                             ( 3.0 IN)
   DISTANCE BETWEEN STAGES - CM
                                                  7.62
   DISTANCE BETWEEN VANES - CM
                                                  2.5
                                                             ( 1.00 IN)
                                                   . 2
                                                             ( 1.0 IN-H20)
   PRESSURE DROP KPA
   SUPERFICAL GAS VELOCITY - M/S
                                                  4.6
                                                              ( 15.0 FT/S)
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                            STAINLESS STEEL
                                              AUSTENITIC
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LOUISVILLE GAS & ELECTRIC: MILL CREEK 4 (CONT.)

LUUI	SVILLE GAS & CELETRIES HEEL GREEK ! (GGHT).	
	WASH WATER SOURCE Wash Rate - L/S	FRESH 2.5 (40 GAL/MIN)
**	REHEATER NUMBER NUMBER OF SPARES NUMBER PER MODULE GENERIC TYPE SPECIFIC TYPE TRADE NAME/COMMON TYPE CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE	4 0 1 IN-LINE STEAM BARE TUBE CAREON STEEL AISI 1110
**	FANS NUMBER NUMBER OF SPARES DESIGN SUPPLIER FUNCTION APPLICATION SERVICE FLUE GAS FLOW RATE - CU.M/S FLUE GAS TEMPERATURE - C PRESSURE DROP - KPA CONSTRUCTION MATERIAL GENERIC TYPE	2 0 CENTRIFUGAL AMERICAN STANDARD UNIT FORCED DRAFT DRY 377.52 (800000 ACFM) 148.9 (300 F) 12.9 (42.3 IN-H20) CARBON STEEL
**	DAMPERS NUMBER FUNCTION GENERIC TYPE SPECIFIC TYPE CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	SHUT-OFF GUILLOTINE TOP-ENTRY GUILLOTINE STAINLESS STEEL AUSTENITIC NONE N/A
**	DUCTWORK LOCATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	ABSORBER INLET CARBON STEEL AISI 1110 INORGANIC HYDRAULICALLY-BONDED MORTAR
**	DUCTWORK LOCATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	ABSORBER OUTLET CARBON STEEL AISI 1110 INORGANIC HYDRAULICALLY-BONDED MORTAR
**	DUCTWORK LOCATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	DOWNSTREAM OF REHEATER CARBON STEEL AISI 1110 ORGANIC HYDRAULICALLY-BONDED MORTAR
**	DUCTWORK LOCATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	BYPASS CARBON STEEL AISI 1110 NONE N/A
**	REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE DEVICE TYPE NUMBER	WET BALL MILL COMPARTMENTED NR 1

LOUISVILLE GAS & ELECTRIC: MILL CREEK 4 (CONT.)

	_		_
**	11	١NК	

SERVICE	NUMBER
CARBIDE LIME SLURRY	2
ADDITIVE SLURRY DAY	1
REACTION	4
THICKENER	1

** PUMPS

SERVICE	NUMBER
ADDITIVE SLURRY TRANSFER	7
RECYCLE	10
SCRUEBER BLEED	6
THICKENER	2
NR	****

** SOLIDS CONCENTRATING/DEWATERING

DEVICE THICKENER NUMBER 1 NUMBER OF SPARES 0 DIMENSIONS - FT 125.0 X 10.0 SHELL GENERIC MATERIAL TYPE CARBON STEEL SHELL SPECIFIC MATERIAL TYPE AISI 1110 LINER GENERIC MATERIAL TYPE NR LINER SPECIFIC MATERIAL TYPE NR FEED STREAM CHARACTERISTICS 10% SOLIDS OUTLET STREAM CHARACTERISTICS 20% SOLIDS

*** SALEABLE BYPRODUCTS

NATURE NONE

*** SLUDGE

** TREATMENT

METHOD FIXATION
DEVICE PUG MILL
PROPRIETARY PROCESS CONVERSION SYSTEMS [POZ-O-TEC]

** DISPOSAL

NATURE FINAL
TYPE POND
LOCATION ON-SITE
SITE TRANSPORTATION METHOD PIPELINE
SITE TREATMENT CLAY LINING
SITE DIMENSIONS 100 ACRES

** PROCESS CONTROL AND INSTRUMENTATION

PROCESS STREAM SLURRY RECYCLE
CHEMICAL PARAMETERS PH
MONITOR TYPE UNILOC
MONITOR LOCATION IN REACTION TANK

** WATER BALANCE

WATER LOOP TYPE CLOSED

** CHEMICALS AND CONSUMPTION

FUNCTION ABSORBENT
NAME CARBIDE LIME
PRINCIPAL CONSTITUENT 90% CAOH2
SOURCE/SUPPLIER AIRCO

LOUISVILLE GAS & ELECTRIC: MILL CREEK 4 (CONT.)

PERIOD	MODULE	AVAILABILITY		RELIABILITY	UTILIZATION	% REMOVAL SO2 PART.	PER HOURS	HOURS	HOURS	CAP. FACTOR
~~~~										
7/82	SYSTEM	5.4	21.8	21.8	4.6		744	156	34	50.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS							
		т	HE UTILITY RI	PORTED THAT	START-UP FOR	THE NEW BO	ILER WA	1 NO 2	ULY 15,	1982.
8/82	SYSTEM	41.4	78.5	78.5	41.1		744	390	306	50.0
9/82	SYSTEM	39.4	52.4	52.9	38.5		720	529	277	50.0
10/82	SYSTEM	.0			.0		744	0	0	50.0
11/82	SYSTEM	.0	.0	.0	.0		72 <b>0</b>	347	0	50.0
12/82	SYSTEM	35.1	56.6	56.6	35.1		744	461	261	50.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS							
					PROBLEMS ASS URING THE PER					
1/83	SYSTEM	18.1	24.2	24.2	18.1		744	558	135	50.0
2/83	SYSTEM	.0	.0	.0	.0		672	600	0	50.0
3/83	SYSTEM	25.3	64.4	64.4	24.1		744	278	179	50.0
4/83	SYSTEM	44.7	48.5	48.5	41.3		72 <b>0</b>	612	297	50.0
5/83	SYSTEM	65.2	95.3	95.3	59.4		744	464	442	50.0
6/83	SYSTEM	6.4	7.4	7.4	6.4		720	619	46	50.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS							
			YPASS DAMPER .983.	REPAIRS WER	E MADE DURING	THE PERIOD	OF JAN	WARY TI	HROUGH	JUNE,
			HE UTILITY R		ICKENER RAKE	FAILURE DUR	ING TH	E PERIO	D OF JA	MUARY
			THE UTILITY R	EPORTED REHE	AT PROBLEMS D	URING THE P	ERIOD (	DF JANU	ARY THE	ROUGH
7/83	SYSTEM	37.5	40.7	40.7	36.8		744	673	274	50.0
8/83	SYSTEM	36.6	39.1	39.1	36.6		744	695	272	50.0
9/83	SYSTEM	15.7	15.7	15.7	15.7		720	720	113	50.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS							
					UP IN ACCUMUL N OUTAGE TIME		NER SO	LIDS DU	RING TH	łΕ
			HICKENER UND HE PERIOD.	ERFLOW PUMP	PROBLEMS CONT	RIBUTED TO	LOW AV	AILABIL	ווס אדו	RING

12.4

32.5

THIRD QUARTER.

12.4

32.5

4.8

43.6

10/83 SYSTEM

11/83 SYSTEM

THE UTILITY REPORTED PLUGGING IN THE ABSORBER MOBILE BALL BEDS DURING THE

744 290 36

720 701 228

4.8

31.7

720

LOUISVILLE GAS & ELECTRIC: MILL CREEK 4 (CONT.)

				PERFORMAN	CE DATA			
PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION			
						502 PART.	HOURS HOURS	HOURS FACTOR
12/83	SYSTEM	57.4	45.8	45.8	39.4		744 640	293
	** PRO	BLEMS/SOLUTION	NS/COMMENTS					
		N	O MAJOR FGD-	RELATED PROBI	LEMS WERE REP	PORTED FOR T	HE FOURTH QUA	RTER OF 1983.
1/84	SYSTEM						744	
2/84	SYSTEM						696	
3/84	SYSTEM						744	
4/84	SYSTEM						720	
5/84	SYSTEM						744	
6/84	SYSTEM						720	
7/84	SYSTEM						744	
8/84	SYSTEM						744	

# ** PROBLEMS/SOLUTIONS/COMMENTS

9/84 SYSTEM

INFORMATION WAS UNAVAILABLE FOR THE FIRST THREE QUARTERS OF 1984.

# SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

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LOUISVILLE GAS & ELECTRIC COMPANY NAME PADDY'S RUN PLANT NAME UNIT NUMBER LOUISVILLE CITY STATE KENTUCKY REGULATORY CLASSIFICATION 43. ( .100 LB/MMBTU) 516. ( 1.200 LB/MMBTU) ***** (***** LB/MMBTU) PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J 302 NET PLANT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW 72 GROSS UNIT GENERATING CAPACITY - MW
NET UNIT GENERATING CAPACITY W/FGD - MW
NET UNIT GENERATING CAPACITY WO/FGD - MW 72 67 69 EQUIVALENT SCRUBBED CAPACITY - MW ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER FOSTER WHEELER BOILER TYPE PULVERIZED COAL 174.60 ( 370000 ACFM) 168.3 ( 335 F) 76. ( 250 FT) CONCRETE BOILER SERVICE LOAD DESIGN BOILER FLUE GAS FLOW - CU.M/S BOILER FLUE GAS TEMPERATURE - C STACK HEIGHT - M STACK SHELL 4.3 ( 14.0 FT) STACK TOP DIAMETER - M ** FUEL DATA FUEL TYPE COAL FUEL GRADE BITUMINOUS AVERAGE HEAT CONTENT - J/G 26284. ( 11300 BTU/LB) RANGE HEAT CONTENT - BTU/LB 10400-11900 AVERAGE ASH CONTENT - % 14.00 RANGE ASH CONTENT - % 10.0-20.0 AVERAGE MOISTURE CONTENT - % 9.00 RANGE MOISTURE CONTENT - % 8.0-10.8 AVERAGE SULFUR CONTENT - % 3.70 RANGE SULFUR CONTENT - % 3.5-4.0 AVERAGE CHLORIDE CONTENT - % . 04 RANGE CHLORIDE CONTENT - % .03-.06 *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER TYPE NONE ** ESP NUMBER 1 NUMBER OF SPARES 0 TYPE COLD SIDE SUPPLIER RESEARCH-COTTRELL INLET FLUE GAS CAPACITY - CU.M/S 174.6 ( 370000 ACFM) INLET FLUE GAS TEMPERATURE - C 168.3 ( 335 F) PARTICLE REMOVAL EFFICENCY - % 99.1 ** PARTICLE SCRUBBER HUMBER n GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL N/A LINER GENERIC MATERIAL N/A LINER SPECIFIC MATERIAL N/A GAS CONTACTING DEVICE TYPE N/A

*** FGD SYSTEM

LOUISVILLE GAS & ELECTRIC: PADDY'S RUN 6 (CONT.)

```
** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                             THROWAWAY PRODUCT
   SO2 REMOVAL MODE
                                             WET SCRUBBING
   PROCESS TYPE
                                              LIME
   SYSTEM SUPPLIER
                                              COMBUSTION ENGINEERING
   A-E FIRM
                                              FLUOR - PIONEER
   DEVELOPMENT LEVEL
                                              FULL SCALE
   NEW/RETROFIT
                                              RETROFIT
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.10
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                 90.00
   ENERGY CONSUMPTION - %
                                                  2.8
   CURRENT STATUS
   COMMERCIAL START-UP
                                               4/73
   INITIAL START-UP
                                               4/73
   CONTRACT AWARDED
                                               7/71
** DESIGN AND OPERATING PARAMETERS
                                                 4.00
   DESIGN COAL SULFER CONTENT - %
   DESIGN COAL HEAT CONTENT - J/G
                                              24190.4
                                                            ( 10400 BTU/LB)
   OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                               192.0
** QUENCHER/PRESATURATOR
   NUMBER
                                               Λ
** ABSORBER
   NUMBER
                                               2
   NUMBER OF SPARES
                                              Ω
   GENERIC TYPE
                                              PACKED TOWER
   SPECIFIC TYPE
                                              STATIC BED PACKING
   TRADE NAME/COMMON TYPE
                                             MARBLE-BED SCRUBBER
   SUPPLIER
                                              COMBUSTION ENGINEERING
   DIMENSIONS - FT
                                              17.0 X 18.0 X 50.0
   SHELL GENERIC MATERIAL
                                              CARBON STEEL
   SHELL SPECIFIC MATERIAL
                                              AISI 1110
   SHELL MATERIAL TRADE NAME/COMMON TYPE
                                              N/A
   LINER GENERIC MATERIAL
                                              ORGANIC
   LINER SPECIFIC MATERIAL
                                              GLASS FLAKE-FILLED POLYESTER; MICA FLAKE-FILLED
   LINER MATERIAL TRADE NAME/COMMON TYPE
                                              FLAKELINE 103; FLAKELINE 151
   GAS CONTACTING DEVICE TYPE
                                              GLASS MARBLES
   NUMBER OF CONTACTING ZONES
                                              2
                                              7.6
   DISTANCE BETWEEN GAS CONTACTING ZONES - CM
                                                                3.0IN)
                                                           ( 8100 GPM)
   LIQUID RECIRCULATION RATE LITER/S
                                               510.
                                                           ( 43.8 GAL/1000 ACF)
   L/G RATIO - L/CU.M
                                                5.9
                                                            (11.0 IN-H20)
   GAS-SIDE PRESSURE DROP - KPA
                                                 2.7
   SUPERFICAL GAS VELOCITY - M/SEC
                                                            ( 10.0 FT/S)
                                                 3.0
   INLET GAS FLOW CU. M/S
                                                87.30
                                                           ( 185000 ACFM)
                                                            ( 335 F)
   INLET GAS TEMPERATURE - C
                                               168.3
   SO2 REMOVAL EFFICIENCY %
                                                85.0
                                                 99.0
   PARTICLE REMOVAL EFFICENCY - %
** MIST ELIMINATOR
                                              PRIMARY COLLECTOR
   PRE-MIST ELIMINATOR/MIST ELIMINATOR
   NUMBER PER SYSTEM
                                               4
   NUMBER OF SPARES PER SYSTEM
                                               0
   NUMBER PER MODULE
                                              2
                                              IMPINGEMENT
   GENERIC TYPE
                                              BAFFLE
   SPECIFIC TYPE
   TRADE NAME/COMMON TYPE
                                              CLOSED VANE
                                              COMBUSTION ENGINEERING
   MANUFACTURER
                                              HORIZONTAL
   CONFIGURATION
   NUMBER OF STAGES
   NUMBER OF PASSES PER STAGE
                                                  3
                                                 1.52
                                                            ( 5.0 FT)
   FREEBOARD DISTANCE - M
                                               121.92
                                                            (48.0 IN)
   DISTANCE BETWEEN STAGES CM
   DISTANCE BETWEEN VANES - CM
                                                             ( 1.70 IN)
                                                 4.3
                                                45
   VANE ANGLES DEGREES
   PRESSURE DROP KPA
                                                             ( 1.5 IN-H20)
                                                             ( 10.0 FT/S)
   SUPERFICAL GAS VELOCITY - M/S
                                                  3.0
   CONSTRUCTION MATERIAL GENERIC TYPE
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                             ORGANIC
                                             POLYPROPYLENE
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# LOUISVILLE GAS & ELECTRIC: PADDY'S RUN 6 (CONT.)

EUOISVIELE GAS & ELECTRIST FABRICS ROW & COOK	• •
WASH WATER SOURCE	FRESH
WASH FREQUENCY	EVERY 8 HOURS
WASH RATE - L/S	8.8 ( 140 GAL/MIN)
** REHEATER	
NUMBER	4
NUMBER OF SPARES	0
NUMBER PER MODULE	2
GENERIC TYPE	DIRECT COMBUSTION
SPECIFIC TYPE	IN-LINE BURNER
TRADE NAME/COMMON TYPE	NATURAL GAS
COMBUSTION FUEL SULFER CONTENT - %	.0
LOCATION	IN OUTLET DUCT
PERCENT GAS BYPASSED - AVG	.0
TEMPERATURE INCREASE - C	27.8 ( 50 F)
INLET FLUE GAS TEMPERATURE - C	52.2 ( 126 F)
OUTLET FLUE GAS TEMPERATURE - C	80.0 ( 176 F)
	CAST IRON
CONSTRUCTION MATERIAL SPECIFIC TYPE	NR
VV FALIA	
** FANS	•
NUMBER	1
NUMBER OF SPARES	0
DESIGN	CENTRIFUGAL
SUPPLIER	WESTINGHOUSE
FUNCTION APPLICATION	BOOSTER
	INDUCED DRAFT
SERVICE	DRY ( ) TERMS ACEN'S
FLUE GAS FLOW RATE CU.M/S FLUE GAS TEMPERATURE - C	82.58 ( 175000 ACFM)
	80.0 ( 176 F)
CONSTRUCTION TRATERIAL GENERIC TIPE	CARBON STEEL
** DAMPERS	
NUMBER	7
FUNCTION	CONTROL/SHUT-OFF
GENERIC TYPE	LOUVER
SPECIFIC TYPE	NR
MANUFACTURER	COMBUSTION ENGINEERING
SEAL AIR FLOW - CU. M/S	.00 ( 0 ACFM)
CONSTRUCTION MATERIAL GENERIC TYPE	CARBON STEEL
CONSTRUCTION MATERIAL SPECIFIC TYPE	AISI 1110
LINER GENERIC MATERIAL TYPE	NONE
LINER SPECIFIC MATERIAL TYPE	N/A
** DUCTWORK	
LOCATION	INLET
CONFIGURATION	RECTANGULAR
SHELL GENERIC MATERIAL TYPE	CARBON STEEL
SHELL SPECIFIC MATERIAL TYPE	AISI 1110
LINER GENERIC MATERIAL TYPE	NONE
LINER SPECIFIC MATERIAL TYPE	N/A
VV BUSTION	
** DUCTWORK	
LOCATION	OUTLET
CONFIGURATION	RECTANGULAR
SHELL GENERIC MATERIAL TYPE	CARBON STEEL
SHELL SPECIFIC MATERIAL TYPE	AISI 1110
LINER GENERIC MATERIAL TYPE	NONE
LINER SPECIFIC MATERIAL TYPE	N/A
** DUCTWORK	
LOCATION	TVB.66
CONFIGURATION	BYPASS
SHELL GENERIC MATERIAL TYPE	RECTANGULAR
SHELL SPECIFIC MATERIAL TYPE	CARBON STEEL
LINER GENERIC MATERIAL TYPE	AISI 1110
LINER SPECIFIC MATERIAL TYPE	NONE
STITER SPECIFIC HATERIAL TIPE	N/ <b>A</b>
** REAGENT PREPARATION EQUIPMENT	
FUNCTION EQUIPMENT	COTANTING OF SOLTES FOLKE THE BARGE OF THERES SALE
PRODUCT QUALITY - % SOLIDS	GRINDING OF SOLIDS FOUND IN BARGE DELIVERED CARB 25.0
Y JOETUS	23.0

LOUISVILLE GAS & ELECTRIC: FADDY'S	RUN 6 (CONT.)
** TANKS SERVICE	NUMBER
ABSORBER RECYCLE	AAAA
REAGENT PREP PRODUCT	****
THICKENER OVERFLOW	**** ****
INICKERER OVERFLOW	***
** PUMPS	
SERVICE	NUMBER
52RVICE	NUMBER
RECYCLE	3
ABSORBER BLEED	****
THICKENER UNDERFLOW	2
CARBIDE LIME SLURRY	***
THICKENER OVERFLOW	***
** SOLIDS CONCENTRATING/DEWATERING	
DEVICE	VACUUM FILTER
NUMBER	2
NUMBER OF SPARES	1
CAPACITY	240 TONS/DAY
SHELL GENERIC MATERIAL TYPE	CARBON STEEL
SHELL SPECIFIC MATERIAL TYPE	AISI 1110
LINER GENERIC MATERIAL TYPE	ИR
LINER SPECIFIC MATERIAL TYPE	NR
BELT GENERIC MATERIAL TYPE	ORGANIC
BELT SPECIFIC MATERIAL TYPE	POLYFROPYLENE
FEED STREAM SOURCE	THICKENER UNDERFLOW
FEED STREAM CHARACTERISTICS	23% SOLIDS
OUTLET STREAM CHARACTERISTICS	45-50% SOLIDS
OUTLET STREAM DISPOSITION	LANDFILL
OVERFLOW STREAM DISPOSITION	TO THICKENER
** SOLIDS CONCENTRATING/DEWATERING	
DEVICE	THICKENER
NUMBER	1
NUMBER OF SPARES	0
DIMENSIONS - FT	50 DIA X 17.0
CAPACITY	250000
SHELL GENERIC MATERIAL TYPE	CARBON STEEL
SHELL SPECIFIC MATERIAL TYPE	AISI 1110
LINER GENERIC MATERIAL TYPE	NONE
LINER SPECIFIC MATERIAL TYPE	N/A
FEED STREAM SOURCE	ABSORBER BLEED
FEED STREAM CHARACTERISTICS	10% SOLIDS
OUTLET STREAM CHARACTERISTICS	23% SOLIDS VACUUM FILTER
OUTLET STREAM DISPOSITION OVERFLOW STREAM DISPOSITION	TO REACTION TANK
OVERTEEN STREAM DISPOSITION	TO THE STATE OF TH
*** SLUDGE	
% CASO3 - DRY	96.0
% CASO4 - DRY	4.0
% ASH - DRY	3.5
** TREATMENT	
METHOD	FIXATION
DEVICE	LANDFILL
PROPRIETARY PROCESS	NONE
INLET QUALITY - %	40.0
** DISPOSAL	
NATURE	FINAL

NATURE

LOCATION

SITE TRANSPORTATION METHOD SITE TREATMENT

TYPE

FINAL

TRUCK NONE

LANDFILL

OFF-SITE

LOUISVILLE GAS & ELECTRIC: PADDY'S RUN 6 (CONT.)

** PROCESS CONTROL AND INSTRUMENTATION

MAKEUP WATER ADDITION - LITERS/S

PROCESS STREAM CHEMICAL PARAMETERS CONTROL LEVELS

INLET, OVERFLOW POT DRAINS, SUMP

PH <6 UPPER BED, PH >4 LOWER BED, PH 8-10 AT INL

** WATER BALANCE

WATER LOOP TYPE

CLOSED

3.1 ( 50 GPM)

** CHEMICALS AND CONSUMPTION

FUNCTION NAME PRINCIPAL CONSTITUENT SOURCE/SUPPLIER CONSUMPTION POINT OF ADDITION

ABSORBENT CARBIDE LIME CAIOH12 AIRCO

4800 LB/HR DRY CAIOH12 ADDITIVE SLURRY TANK

** FGD SPARE CAPACITY INDICES

ABSORBER - % MIST ELIMINATOR - % REHEATER - % FAN - 2 EFFLUENT HOLD TANK - % RECIRCULATION PUMP - % THICKENER - % VACUUM FILTER - % ** FGD SPARE COMPONENT INDICES 20.0 .0 .0 .0 . 0 33.0 .0 .0

ABSOPBER MIST ELIMINATOR REHEATER FAN EFFLUENT HOLD TANK RECIRCULATION PUMP THICKENER VACUUM FILTER

.0 . 3 . 0 .0 .0 1.0 .0 .0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

4/73 6A 18.0 8.0 6B 56.0 24.9 720 SYSTEM 37.0 16.5

** PROBLEMS/SOLUTIONS/COMMENTS

INITIAL OPERATION OF THE FGD SYSTEM AT PADDY'S RUN BEGAN IN APRIL. THE MODULES WERE OPERATED ONE AT A TIME, WITH FREQUENT SHUTDOWNS FOR INSPEC-TION OF EQUIPMENT AND MINOR REPAIRS.

320

265

255

744

720

118

101

A

5/73 6A 11.0 3.9 6B 65.0 23.1 SYSTEM 38.0 13.5

** PROBLEMS/SOLUTIONS/COMMENTS

SINGLE-MODULE OPERATION CONTINUED THROUGH MAY 19, WHEN THE UNIT WAS SHUT DOWN FOR MODIFICATIONS.

EQUIPMENT WAS INSTALLED FOR INJECTION OF A FLOCCULATING AGENT INTO THE CLARIFIER TANK.

6/73 6A .0 .1 6B 6.0 2.1 SYSTEM 7 . 7

3.1

		SILITY OPERABILITY RELIABI		S02	PART.	HOURS	HOURS	HOURS	FACTO	
7/73	6A	21.0	6.7							
///3	6B	21.0	6.7							
	SYSTEM	21.0	6.7			744	240	50		
	** PROBLEMS/SO	DLUTIONS/COMMENTS								
		DURING A SCHEDULED C WERE MADE TO THE LIM INSTALLED TO REDUCE	IE SLURRY MAKE-UP	SYSTEN	1. A I	DISINT	GRATOR	UNIT	WAS	
		OPERATION WAS INTERM PROBLEMS WITH THE SU		19 TO	JULY	ll BEC	USE OF	MECHA	HICAL	
8/73	6A	53.0	23.5							
	6B	64.0	28.4							
	SYSTEM	58.5	26.0			744	330	193		
	** PROBLEMS/SO	DLUTIONS/COMMENTS								
		THE OPERATION WAS CO SHUTDOWN DUE TO A BO			TO AU	GUST 18	EXCEP	T FOR A	A BRIEF	
		FROM AUGUST 19 TO SE CLARIFIER UNDERFLOW ADDITIONAL PUMP CAPA	LINE WITH ONE OF	LARGER	RAID 9	ETER A	I OT OF			
9/73	6A	85.0	46.1							
	6B	72.0	39.0							
	SYSTEM	78.5	42.6			720	390	306		
	** PROBLEMS/S	DLUTIONS/COMMENTS								
		THE UNIT OPERATED CO 7-HOUR SHUTDOWN TO F					20 EXC	EPT FO	R A	
		THE UNIT WAS SHUT DO	OWN FROM SEPTEMBER	20 TO	THE	END OF	THE MO	нтн.		
10/73	6A	49.0	45.4							
	6B	94.0	87.2							
	SYSTEM	71.5	66.3			744	690	493		
11/73	6A	35.0	35.0							
	6B	100.0	100.0							
	SYSTEM	67.5	67.5			720	720	486		
12/73	6A	44.0	11.3							
	6B SYSTEM	78.0 61.0	19.9 15.6			744	190	116		
		** PROBLEMS/SOLUTIONS/COMMENTS								
		THE FGD SYSTEM WAS ( THE SCRUBBER MODULE: A PEAKING-LOAD BOILE!	S WERE SHUT DOWN E	EMBER BECAUS	20 AF E OF A	TER WH LACK	ICH THE OF DEMA	BOILE	R AND IS IS	
1/74	SYSTEM		.0			744	0	0	.0	
	** PROBLEMS/S	OLUTIONS/COMMENTS								
		THE BOILER WAS SHUT	DOWN DUE TO A LAG	K OF	DEMAND	•				
2/74	SYSTEM		.0			672	0	0	. 0	
3/74	SYSTEM		.0			744	0	0	.0	

LOUISVILLE GAS & ELECTRIC: PADDY'S RUN 6 (CONT.)

					NCE DATA						
PERIOD	MODULE	AVAILABILITY	OPERABILLIT		UIILIZAIIUN				HOURS		CAP. FACTOR
					_	~					
4/74	SYSTEM				.0			720	0	0	. 0
5/74	SYSTEM				. 0			744	0	0	.0
6/74	SYSTEM				.0			720	0	0	.0
7/74	6A 6B		51.0 81.0		21.0 33.3						
	SYSTEM		66.0		27.2			744	306	202	
8/74			50.0		2.1						
	6B SYSTEM		77.0 6 <b>3.5</b>		3.2 2.7			744	31	20	
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			THE UNIT HAS DEMAND.	BEEN ON AND	OFF FREQUENT	LY DU	E TO F	LUCTUA'	TION IN	POWER	
9/74	SYSTEM		.0		.0			720	43	0	
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			THE BOILER WA	AS SHUT DOWN	BECAUSE OF A	LACK	OF DE	MAND.			
10/74	6A 6B		100.0 100.0		32.9 32.9						
	SYSTEM		100.0		32.9			744	245	245	
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			THE BOILER WA	AS OPERATED	TO PERFORM LI	MESTO	NE TES	TS 0N	THE FGD	SYSTE	1.
11/74	SYSTEM		.0		.0			720	122	0	
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			THE BOILER W	AS SHUT DOWN	BECAUSE OF A	LACK	OF DE	MAND.			
12/74	SYSTEM				.0			744	0	0	.0
1/75	SYSTEM				.0			744	0	0	.0
2/75	SYSTEM				.0			672	0	0	.0
3/75	SYSTEM				.0			744	0	0	.0
4/75	SYSTEM				.0			720	0	0	.0
5/75	SYSTEM				.0			744	0	0	.0
6/75	SYSTEM				.0			720	0	0	.0
7/75	SYSTEM				.0			744	0	0	.0
8/75	SYSTEM				.0			744	0	0	.0
9/75			100.0		100.0						
	6B System	100.0	100.0 100.0		100.0 100.0			720	720	720	
10/75	6A		100.0		100.0			•	,	•	

LOUISVILLE GAS & ELECTRIC: PADDY'S RUN 6 (CONT.)

 			PERFORMA	NCE DATA						
	AVAILABILITY									
					502	PART.	HOURS	HOURS	HOURS	FACTOR
6B		100.0		100.0						
SYSTEM	100.0	100.0		100.0			744	744	744	

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER AND FGD SYSTEM WERE OPERATIONAL ALL OF SEPTEMBER AND THE FIRST TWO WEEKS IN OCTOBER. OPERABILITY FOR BOTH MODULES DURING THE OPERATIONAL PERIOD WAS 100% (BASED UPON LG&E'S PEAK LOAD DETERMINATION). SO2 REMOVAL WAS REPORTED TO BE OVER 98%.

SYSTEM OUTAGE IN THE LAST TWO WEEKS OF OCTOBER WAS DUE PRIMARILY TO PROBLEMS WITH THE BREECHING IN THE BOILER SECTION.

11/75	6 <b>A</b>		100.0	100.0			
	6B		100.0	100.0			
	SYSTEM	100.0	100.0	100.0	72 <b>0</b>	720	720

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER AND SCRUBBER SYSTEM OPERATED MOST OF THE REPORT PERIOD ON A MONDAY-FRIDAY BASIS.

12/75	6A	90.1	90.1			
	6B	90.1	90.1			
	SYSTEM	90.1	90.1	744	744	670

### ** PROBLEMS/SOLUTIONS/COMMENTS

TWO MINOR OUTAGES IN DECEMBER WERE DUE TO MALFUNCTION AND REPAIR OF THE DUAL STRAINER SWITCH SHAFT IN THE BOTTOM OF THE SCRUBBER MODULE.

1/76 SYSTEM 53.5 18.7 744 260 139

** PROBLEMS/SOLUTIONS/COMMENTS

SO2 REMOVAL EFFICIENCY WAS REPORTED TO BE 99% DURING JANUARY.

2/76 SYSTEM 66.7 9.8 696 102 68

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE SYSTEM WAS SHUTDOWN IN EARLY FEBRUARY IN PREPARATION FOR AN EXTENSIVE SLUDGE STUDY TO MONITOR FIXATION, LEACHATES, AND SEASONAL VARIATIONS. THE STUDY IS SCHEDULED TO BEGIN IN JUNE OR JULY. THE SCRUBBER WILL NOT BE OPERATED UNTIL THE START OF THE PROGRAM UNLESS THE BOILER IS REQUIRED FOR PEAKING POWER DEMANDS, HIGHLIGHTS OF THE SCRUBBER/SLUDGE STUDY PROGRAM ARE AS FOLLOWS:

- -SIX MONTHS DURATION.
- -ONE SCHEDULED SHUTDOWN FOR TEST MODIFICATIONS.
- -DELIBERATE HIGH CHLORIDE CONCENTRATION OPERATION.
- -MGO INNOCULATION.

3/76 SYSTEM .0 744 0 0 .0

# ** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT REMAINED OFF LINE DURING MARCH IN PREPARATION FOR THE EPA SCRUBBER/SLUDGE STUDY. THE UTILITY IS NOW COMPLETING SYSTEM MODIFICATIONS NECESSARY FOR THE OPERATION OF THE TEST PROGRAM.

4/76	SYSTEM	.0	.0	720	2	0
5/76	SYSTEM	85.0	2.3	744	20	17
6/76	SYSTEM	95.0	21.3	720	161	153

LOUISVILLE GAS & ELECTRIC: PADDY'S RUN 6 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

### ** PROBLEMS/SOLUTIONS/COMMENTS

THIS PEAK LOAD UNIT WAS OPERATED PART OF THE TIME DURING THE REPORT PERIOD (APPROXIMATELY 2 WEEKS IN MAY AND TWO WEEKS IN JUNE). THE SCRUEBER WAS AVAILABLE TO THE BOILER 100% OF THE TIME AND SO2 REMOVAL EFFICIENCY WAS 98 TO 99% DURING THIS OPERATING SEGMENT.

7/76	SYSTEM	87.7	30.8	744	261	229
8/76	SYSTEM	92.8	8.6	744	69	64

### ** PROBLEMS/SOLUTIONS/COMMENTS

THIS UNIT WAS OPERATIONAL PART OF THE TIME DURING THE JULY-AUGUST PERIOD. THE SCRUBBING SYSTEM WAS AVAILABLE TO THE BOILER ON A 100% BASIS. NO MAJOR SCRUBBER-RELATED PROBLEMS WERE ENCOUNTERED.

9/76	SYSTEM		.0	720	0	0	.0
10/76	SYSTEM	94.6	21.2	744	167	158	

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT DID NOT OPERATE THROUGHOUT SEPTEMBER AND THE FIRST THREE WEEKS IN OCTOBER. THE EPA-FUNDED SCRUBBER/SLUDGE STUDY PROGRAM COMMENCED OCTOBER 25. THE INITIAL PHASE OF THE PROGRAM CALLS FOR OPERATIONS TO PROCEED FOR A 20-30 DAY PERIOD WITH CARBIDE LIME SCRUBBING ABSORBENT. FOLLOWING COMPLETION OF THIS RUN, THE UNIT WILL BE SHUT DOWN AND MODIFICATIONS WILL BE INCORPORATED INTO THE SYSTEM FOR OPERATION WITH COMMERCIAL GRADE (HIGH CALCIUM) LIME.

715

11/76 SYSTEM 99.3 99.3 720 720

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS IN SERVICE DURING THE REPORT PERIOD. THE SCRUBBING SYSTEM OPERATED 99.5% OF THE TIME THAT THE BOILER WAS IN SERVICE. CARBIDE LIME WAS EMPLOYED AS THE SO2 ABSORBENT. THE HIGH CALCIUM (VIRGIN) LIME RUN, SCHEDULED AS PART OF THE SCRUBBER/SLUDGE STUDY, WILL COMMENCE ON MARCH 1, 1977.

12/76 SYSTEM 98.5 71.4 744 539 531

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS IN SERVICE DURING THE REPORT PERIOD. THE SCRUBBING SYSTEM OPERATED 99.5% OF THE TIME THAT THE BOILER WAS IN SERVICE. CARBIDE LIME WAS EMPLOYED AS THE SO2 ABSORBENT. THE HIGH CALCIUM (VIRGIN) LIME RUN, SCHEDULED AS PART OF THE SCRUBBER/SLUDGE STUDY, WILL COMMENCE ON MARCH 1, 1977.

1/77	SYSTEM	.0	.0	744	103	0
2/77	SYSTEM	.0	.0	672	62	0
3/77	SYSTEM	79.2	41.4	744	389	308

# ** PROBLEMS/SOLUTIONS/COMMENTS

BECAUSE OF SEVERE WEATHER CONDITIONS THERE WERE NO BOILER OPERATIONS AND NO SCRUBBER OPERATIONS (SINCE DECEMBER 31) UNTIL MARCH 15, 1977.

4/77 SYSTEM 93.6 42.6 720 328 307

PERFORMANCE DATA	
PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZA	TION % REMOVAL PER BOILER FGD CAP.
	SO2 PART. HOURS HOURS HOURS FACTOR
5/77 SYSTEM 42.5 16.	0 744 280 119

### ** PROBLEMS/SOLUTIONS/COMMENTS

IN MID MARCH LG&E BEGAN TESTS FOR EPA WITH REGULAR LIME SINCE ONE OF THE OBJECTIVES OF THE TEST WAS TO DETERMINE WHETHER THERE WERE APPRECIABLE DIFFERENCES BETHEEN REGULAR LIME AND CARBIDE LIME AT THIS FACILITY. DURING OPERATION WITH REGULAR LIME, SCALING PROBLEMS OCCURRED, INDICATING THAT THE SCALING RESULTED FROM INCREASED OXIDATION LEVELS. AVAILABLE OPTIONS FOR CONTROLLING SCALING WERE LIMITED BY THE FIXED DESIGN FEATURES OF THE SCRUBBER HARDWARE. THE OPTION SELECTED WAS ADDITION OF MGO TO THE SCRUBBING MEDIUM. WHEN MGO WAS ADDED, THE SCALING PROBLEM WAS ELIMINATED, ALLOWING COMPLETION OF THE TEST PROGRAM.

6/77 SYSTEM

93.4

43.3

720 334 312

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE SCRUBBER/SLUDGE EVALUATION STUDY CONTINUED DURING THE PERIOD. THE SCRUBBER PLANT (ONE MODULE IS BEING UTILIZED FOR THIS EXPERIMENTAL PROGRAM) WAS IN SERVICE ON A VIRTUALLY CONTINUOUS BASIS FROM JUNE 18 TO AUGUST 8 OPERATING ON MAGNESIUM INNOCULATED COMMERCIAL LIME. SYSTEM OPERABILITY DURING THIS PERIOD WAS APPROXIMATELY 96%. SO2 REMOVAL EFFICIENCY WAS MEASURED IN EXCESS OF 99.5%. THE SYSTEM WAS SHUT DOWN AT THIS POINT TO PERFORM A NUMBER OF SCHEDULED MODIFICATIONS TO THE SYSTEM FOR TEST PURPOSES. SPECIFICALLY, MODIFICATIONS ARE BEING IMPLEMENTED TO THE SYSTEM IN ORDER TO BYPASS THE REACTION TANK SO A SHORT TERM RETENTION TIME TEST COULD BE CONDUCTED. THE TESTING WAS COMPLETED IN AUGUST 1977 AFTER THE MODIFICATIONS WERE MADE.

7/77	SYSTEM	96.9	95.8	744	736	713
8/77	SYSTEM	94.0	73.5	744	582	547
9/77	SYSTEM	25.9	5.8	720	162	42

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT IS CURRENTLY NOT OPERATING DUE TO THE LACK OF POWER REQUIREMENT.

10/77	SYSTEM	46.9	2.0	744	32	15	
11/77	SYSTEM		. 0	720	0	0	.0
12/77	SYSTEM		.0	744	0	0	.0
1/78	SYSTEM		.0	744	0	0	.0
2/78	SYSTEM		.0	672	0	0	. 0
3/78	SYSTEM		.0	744	0	0	.0

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS OUT OF SERVICE FROM NOVEMBER THROUGH MARCH IN PART BECAUSE OF LOW DEMAND AND IN PART AS A RESULT OF PROBLEMS RELATED TO COLD WEATHER.

4/78	SYSTEM		.0	720	0	0	.0
5/78	SYSTEM		.0	744	0	0	.0
6/78	SYSTEM	98.1	7.1	720	52	51	

LOUISVILLE GAS & ELECTRIC: PADDY'S RUN 6 (CONT.)

PERIOD	MODULE AVAILABILI	TY OPERABILITY RELIABI			PER	BOILER		
	** PROBLEMS/SOLUT	TIONS/COMMENTS						
		PADDY'S RUN WAS ON L OPERATIONAL PROBLEMS				RIOD.	Ю	
7/78	SYSTEM	99.5	25.4		744	190	189	
	** PROBLEMS/SOLUT	TIONS/COMMENTS						
		THE UNIT RAN INTERMI	TTENTLY FOR ABOUT	EIGHT TO T	EN DAYS	OVER	THIS PE	RIOD.
8/78	SYSTEM		.0		744	0	0	.0
9/78	SYSTEM	100.0	47.1		720	339	339	
	** PROBLEMS/SOLUT	TIONS/COMMENTS						
		THIS UNIT WAS OPERAT NEW FLOCCULANT COULD DETERMINE THE TYPE OOTHER LG&E UNITS.	BE CARRIED OUT.	THE RESULT	S OF TH	ESE TE	STS WIL	.L
10/78	SYSTEM		. 0		744	0	0	.0
11/78	SYSTEM		.0		720	0	0	.0
	** PROBLEMS/SOLUT	TIONS/COMMENTS						
		THE BOILER WAS NOT O	PERATED DURING OC	TOBER OR NO	VEMBER.			
12/78	SYSTEM		.0		744	0	0	.0
1/79	SYSTEM		.0		744	0	0	.0
	** PROBLEMS/SOLUT	TIONS/COMMENTS						
		THE UNIT WAS NOT OPE	RATED DURING DECE	MBER OR JAN	WARY.			
2/79	SYSTEM		.0		672	0	0	.0
3/79	SYSTEM		.0		744	0	0	.0
4/79	SYSTEM		.0		720	0	0	.0
	** PROBLEMS/SOLUT	TIONS/COMMENTS						
		THE UNIT WAS NOT OPER	ATED DURING THESE	MONTHS BEC	AUSE O	LACK	OF DEMA	. מא
5/79	SYSTEM		.0		744	0	0	.0
6/79	SYSTEM		. 0		720	0	0	.0
	** PROBLEMS/SOLUT	TIONS/COMMENTS						
		THE UTILITY REPORTED TO INSUFFICIENT DEMAN		NOT OPERAT	E DURI	NG MAY	OR JUNI	E DUE
7/79	SYSTEM	.0	.0		744	19	0	
8/79	SYSTEM	45.0	13.0		744	218	99	
9/79	SYSTEM	.0	.0		720	36	0	

PERIOD			TY OPERABILITY RELIABILITY			PER I			CAP. FACTOR
	** PROBLEMS	/SOLUT	IONS/COMMENTS						
			NO PROBLEMS WERE REPORT THIRD QUARTER 1979.	ED WITH RESPECT	TO OPERATI	ON AT TI	HIS UN	IT DURI	NG THE
10/79	SYSTEM			. 0		744	0	0	.0
11/79	SYSTEM			.0		720	0	0	.0
12/79	SYSTEM			.0		744	0	0	.0
	** PROBLEMS	/SOLUT	IONS/COMMENTS						
			THE UNIT DID NOT OPERAT LACK OF DEMAND.	E DURING THE FO	OURTH QUARTE	R OF 19	79 BECA	AUSE OF	THE
1/80	SYSTEM			.0		744	0	0	. 0
2/80	SYSTEM			.0		696	0	0	. 0
3/80	SYSTEM			.0		744	0	0	.0
	** PROBLEMS	/SOLUT	IONS/COMMENTS						
			THIS UNIT DID NOT OPERA QUARTER OF 1980 DUE TO UNIT AND WILL BE RETIRE	A LACK OF DEMAN	VD. THIS UN				
4/80	SYSTEM	100.0		.0		720	0	0	.0
	** PROBLEMS	.∕S0LUT	IONS/COMMENTS						
			DURING APRIL THE FGD SY OPERATED DUE TO A BOILE			THE TI	ME BUT	WAS NO	T
5/80	SYSTEM	100.0	86.6 86.6	7.8		744	67	58	
	** PROBLEMS	SOLUT	IONS/COMMENTS						
			DURING MAY, NINE HOURS THE LIME SLURRY.	OF OUTAGE TIME	RESULTED FR	OM THE	UNAVAI	LABLITY	OF.
6/80	SYSTEM	100.0	94.1 94.1	6.7		720	51	48	
	** PROBLEMS	/S0LUT	IONS/COMMENTS						
			THE THREE HOURS THE SCR THAT THE BOILER WAS BRO ON DUTY.	UBBERS DID NOT UGHT ON LINE BE	OPERATE IN EFORE THE SC	JUNE WAS RUBBER (	S DUE 1	TO THE DRS WER	FACT !E
7/80		100.0		.0					
		100.0 100.0		.0 .0		744	0	0	.0
	** PROBLEMS	/SOLUT	IONS/COMMENTS						
			THE BOILER AND FGD SYST A LACK OF DEMAND.	EM DID NOT OPER	RATE DURING	THE MON	TH OF	JULY DU	JE TO
8/80	SYSTEM	100.0		. 0		744	0	0	.0
9/80	SYSTEM	100.0		.0		720	0	0	. 0

LOUISVILLE GAS & ELECTRIC: PADDY'S RUN 6 (CONT.)

PERIOD	MODULE A	VAILABILI	TY OPERABILITY RELIABILITY UTILIZATION				BOILER HOURS		CAP.
	** PROBL	EMS/SOLUT	IONS/COMMENTS						
			THE BOILER DID NOT OPERATE DURING AUG WAS AVAILABLE 100% OF THE TIME.	GUST AND	SEPTI	EMBER.	THE FO	GD SYS	TEM
10/80	SYSTEM	100.0	.0			744	0	0	.0
11/80	SYSTEM	100.0	.0			720	0	0	.0
12/80	SYSTEM	100.0	.0			744	0	0	.0
	** PROBL	EMS/SOLUT	IONS/COMMENTS						
			THE UNIT WAS NOT OPERATED DURING THE OF DEMAND.	FOURTH	QUARTI	ER 1981	DUE TO	THE I	_ACK
1/81	SYSTEM	100.0	.0			744	0	0	.0
2/81	SYSTEM	100.0	.0			672	0	0	.0
3/81	SYSTEM	100.0	.0			744	0	0	.0
	** PROBL	EMS/SOLUT	IONS/COMMENTS						
			DURING THE FIRST QUARTER 1981 THE UNDERSAND.	IT WAS N	OT OP	ERATED	DUE TO	THE LA	ACK OF
4/81	SYSTEM	100.0	.0			720	0	0	.0
5/81	SYSTEM	100.0	.0			744	0	0	.0
6/81	SYSTEM	100.0	.0			720	0	0	.0
	** PROBL	.EMS/SOLUT	IONS/COMMENTS						
			THROUGHOUT THE SECOND QUARTER 1981 THE FGD SYSTEM WAS AVAILABLE 100%.	HE BOILE	R DID	NOT O	PERATE;	HOWEV	ER,
7/81	SYSTEM	100.0	.0			744	0	0	.0
8/81	SYSTEM	100.0	.0			744	0	0	.0
9/81	SYSTEM	100.0	.0			720	0	0	.0
	** PROBL	EMS/SOLUT	IONS/COMMENTS						
			PADDY'S RUN UNIT 6 REMAINED OFF LINE	DURING	THE T	HIRD Q	UARTER	1981.	
10/81	SYSTEM	100.0	.0			744	0	0	
11/81	SYSTEM	100.0	.0			720	0	0	
12/81	SYSTEM	100.0	.0			744	0	0	
	** PROBL	EMS/SOLUT	IONS/COMMENTS						
			THROUGHOUT THE FOURTH QUARTER THE FG HOWEVER, THE BOILER WAS NOT NEEDED.	D SYSTEM	1 WAS	AVAILA	BLE FOR	OPERA	TION;
1/82	SYSTEM	100.0	.0			744	744	0	
2/82	SYSTEM	100.0	.0			672	0	0	.0
3/82	SYSTEM	100.0	.0			744	0	0	.0

PERIOD	MODULE AV	AILABILI	TY OPERABILITY RELIABILITY UTILIZATION	% REMOVAL SO2 PART.	PER HOURS	HOURS	HOURS	
	** PROBLE	MS/SOLUT	IONS/COMMENTS					
			DURING THE FIRST QUARTER 1982 THE FGD HOWEVER, THE SYSTEM WAS NOT NEEDED DUE					ION;
4/82	SYSTEM	100.0	.0		720	0		.0
5/82	SYSTEM	100.0	.0		744	0	0	.0
6/82	SYSTEM	100.0	.0		720	0	0	.0
	** PROBLE	MS/SOLUT	IONS/COMMENTS					
			DUE TO A LACK OF POWER DEMAND, THE UNI QUARTER 1982.	T DID NOT O	PERATE	DURING	THE SE	COND
7/82	SYSTEM	100.0	.0		744	0	0	.0
8/82	SYSTEM	100.0	.0		744	0	0	.0
9/82	SYSTEM	100.0	.0		720	0	0	.0
10/82	SYSTEM	100.0	.0		744	0	0	.0
11/82	SYSTEM	100.0	• 0		720	0	0	.0
12/82	SYSTEM	100.0	.0		744	0	0	.0
1/83	SYSTEM	100.0	.0		744	0	0	.0
2/83	SYSTEM	100.0	.0		672	0	0	.0
3/83	SYSTEM	100.0	.0		744	0	0	.0
4/83	SYSTEM	100.0	.0		720	0	0	.0
5/83	SYSTEM	100.0	.0		744	0	0	.0
6/83	SYSTEM	100.0	.0		720	0	0	.0
	** PROBLI	EMS/SOLUT	TIONS/COMMENTS					
			THE UTILITY REPORTED THAT THE UNIT AND THE PERIOD OF JULY 1, 1982 THROUGH JUN REPORTED AVAILABLE 100% OF THE TIME.	FGD SYSTEM E 30, 1983.	THE	OT OPER FGD SYS	ATE DU	RING S
7/83	SYSTEM	100.0	.0		744	0	0	.0
8/83	SYSTEM	100.0	.0		744	0	0	.0
9/83	SYSTEM	100.0	.0		720	0	0	.0
	** PROBLI	EMS/SOLU	TIONS/COMMENTS					
			THE UNIT AND FGD SYSTEM DID NOT OPERAL HOWEVER, THE FGD SYSTEM WAS REPORTED	TE DURING TH TO BE 100% A	E THIR	D QUART	TER OF	1983,
10/83	SYSTEM	100.0	.0		744	0	0	.0
11/83	SYSTEM	100.0	.0		720	0	0	.0
12/83	SYSTEM	100.0	.0		744	0	0	.0

LOUISVILLE GAS & ELECTRIC: PADDY'S RUN 6 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT THE UNIT AND SCRUBBER DID NOT OPERATE DURING THE FOURTH QUARTER OF 1983.

1/84	SYSTEM	744
2/84	SYSTEM	696
3/84	SYSTEM	744
4/84	SYSTEM	720
5/84	SYSTEM	744
6/84	SYSTEM	720
7/84	SYSTEM	744
8/84	SYSTEM	744
9/84	SYSTEM	720

### ** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE FIRST THREE QUARTERS OF 1984.

# SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

	MARQUETTE BOARD OF LIGHT A DIED
COMPANY NAME	MARQUETTE BOARD OF LIGHT & PWR
PLANT NAME	SHIRAS
UNIT NUMBER	3
CITY	MARQUETTE
STATE	MICHIGAN
REGULATORY CLASSIFICATION	В
PARTICULATE EMISSION LIMITATION - NG/J	13. ( .030 LB/MMBTU)
SO2 EMISSION LIMITATION - NG/J	172. ( .400 LB/MMBTU)
NOX EMISSION LIMITATION - NG/J	215. ( .500 LB/MMBTU)
NET PLANT GENERATING CAPACITY - MW	40
GROSS UNIT GENERATING CAPACITY - MW	44
NET UNIT GENERATING CAPACITY W/FGD - MW	495
NET UNIT GENERATING CAPACITY WO/FGD - MW	495
EQUIVALENT SCRUBBED CAPACITY - MW	44
ENGLANCE III SCHOODED CHINCIII III	**
** UNIT DATA - BOILER AND STACK	
BOILER SUPPLIER	COMBUSTION ENGINEERING
	PULVERIZED COAL
BOILER TYPE	
BOILER SERVICE LOAD	BASE
DESIGN BOILER FLUE GAS FLOW - CU.M/S	92.63 ( 196292 ACFM)
BOILER FLUE GAS TEMPERATURE - C	68.3 ( 155 F)
STACK HEIGHT - M	107. ( 350 FT)
STACK SHELL	CONCRETE
STACK TOP DIAMETER - M	2.7 ( 9.0 FT)
** FUEL DATA	
FUEL TYPE	COAL
FUEL GRADE	SUBBITUMINOUS
AVERAGE HEAT CONTENT - J/G	20129. ( 8654 BTU/LB)
RANGE HEAT CONTENT - BTU/LB	****
AVERAGE ASH CONTENT - %	10.25
RANGE ASH CONTENT - %	*****
AVERAGE MOISTURE CONTENT - %	23.42
RANGE MOISTURE CONTENT - %	*****
AVERAGE SULFUR CONTENT - %	.30
RANGE SULFUR CONTENT - %	*****
	**************************************
AVERAGE CHLORIDE CONTENT - %	*****
RANGE CHLORIDE CONTENT - %	
*** PARTICLE CONTROL	
AND PARTICLE CONTROL	
** FABRIC FILTER	
NUMBER	1
	GE ENVIRONMENTAL SERVICES
SUPPLIER	1.7 (6.8 IN-H20)
PRESSURE DROP - KPA	99.8
PARTICLE REMOVAL EFFICENCY - %	.6 ( 2.0 FT/MIN)
TYPICAL GAS/CLOTH RATIO - M/MIN	.6 ( 2.0 11/11211)
XX BARTICLE CONUNCER	
** PARTICLE SCRUBBER	0
NUMBER	
GENERIC TYPE	NONE
SPECIFIC TYPE	N/A
TRADE NAME/COMMON NAME	N/A
SHELL GENERIC MATERIAL	N/A
SHELL SPECIFIC MATERIAL	N/A
LINER GENERIC MATERIAL	N/A
LINER SPECIFIC MATERIAL	N/A
GAS CONTACTING DEVICE TYPE	N/A
*** FGD SYSTEM	
** GENERAL DATA	
SALEABLE PRODUCT/THROWAWAY PRODUCT	THROWAWAY PRODUCT
SO2 REMOVAL MODE	SPRAY DRYING
	LIME/SPRAY DRYING
PROCESS TYPE	GE ENVIRONMENTAL SERVICES
SYSTEM SUPPLIER	LUTZ, DALY, & BRAIN
A-E FIRM	
DEVELOPMENT LEVEL	FULL SCALE
NEW/RETROFIT	NEM

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MARQUETTE BOARD OF LIGHT & PWR: SHIRAS 3 (CONT.)
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UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.80
UNIT DESIGN SO2 REMOVAL EFFICIENCY - % 80.00
CURRENT STATUS 1
COMMERCIAL START-UP 4/83
INITIAL START-UP 3/83
CONTRACT AWARDED 10/80

** DESIGN AND OPERATING PARAMETERS

DESIGN COAL SULFER CONTENT - % .60

### ** QUENCHER/PRESATURATOR

CONSTRUCTION MATERIAL GENERIC TYPE NR
CONSTRUCTION MATERIAL SPECIFIC TYPE NR

### ** ABSORBER

GENERIC TYPE SPRAY DRYER SPECIFIC TYPE TRADE NAME/COMMON TYPE ROTARY ATOMIZER 35'6" DIAMETER DIMENSIONS - FT SHELL GENERIC MATERIAL ND SHELL SPECIFIC MATERIAL NR SHELL MATERIAL TRADE NAME/COMMON TYPE NR LINER GENERIC MATERIAL NONE LINER SPECIFIC MATERIAL N/A LINER MATERIAL TRADE NAME/COMMON TYPE N/A INLET GAS TEMPERATURE - C 129.4

INLET GAS TEMPERATURE - C 129.4 ( 265 F)
SO2 REMOVAL EFFICIENCY - % 80.0
PARTICLE REMOVAL EFFICENCY - % 99.9

### ** MIST ELIMINATOR

PRE-MIST ELIMINATOR/MIST ELIMINATOR

GENERIC TYPE

SPECIFIC TYPE

N/A

TRADE NAME/COMMON TYPE

CONSTRUCTION MATERIAL GENERIC TYPE

NR

CONSTRUCTION MATERIAL SPECIFIC TYPE

NR

### ** REHEATER

GENERIC TYPE
SPECIFIC TYPE
COLD SIDE
TRADE NAME/COMMON TYPE
PERCENT GAS BYPASSED - AVG
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
NR
CONSTRUCTION MATERIAL SPECIFIC TYPE
NR

### ** FANS

DESIGN NR
FUNCTION NR
APPLICATION NR
SERVICE NR
CONSTRUCTION MATERIAL GENERIC TYPE NR

### ** DAMPERS

FUNCTION NR
GENERIC TYPE NR
SPECIFIC TYPE NR
CONSTRUCTION MATERIAL GENERIC TYPE NR
CONSTRUCTION MATERIAL SPECIFIC TYPE NR
LINER GENERIC MATERIAL TYPE NR
LINER SPECIFIC MATERIAL TYPE NR

## ** DUCTWORK

SHELL GENERIC MATERIAL TYPE NR
SHELL SPECIFIC MATERIAL TYPE NR
LINER GENERIC MATERIAL TYPE NR
LINER SPECIFIC MATERIAL TYPE NR

### ** REAGENT PREPARATION EQUIPMENT

FUNCTION SLAKER
DEVICE NR
DEVICE TYPE NR

MARQUETTE BOARD OF LIGHT & PWR: SHIRAS 3 (CONT.)

** PUMPS

SERVICE NUMBER

** SOLIDS CONCENTRATING/DEWATERING

DEVICE

*** SLUDGE

** TREATMENT

METHOD N/A
DEVICE N/A
PROPRIETARY PROCESS N/A

** DISPOSAL

NATURE FINAL
TYPE LANDFILL
LOCATION OFF-SITE
SITE TREATMENT NR

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

3/83 SYSTEM 744

### ** PROBLEMS/SOLUTIONS/COMMENTS

INITIAL START-UP FOR THE FGD SYSTEM OCCURRED DURING MARCH, 1983.

 4/83
 SYSTEM
 720

 5/83
 SYSTEM
 744

 6/83
 SYSTEM
 720

### ** PROBLEMS/SOLUTIONS/COMMENTS

COMMERCIAL OPERATIONS COMMENCED ON APRIL 1, 1983. THE FGD SYSTEM IS PRESENTLY IN THE DEBUGGING PHASE OF OPERATION. NO PERFORMANCE OR WARRANTY TESTS HAVE BEEN RUN.

THE UTILITY REPORTED EXPERIENCING PROBLEMS WITH MATERIAL BUILD UP ON THE SPRAY DRYER WALLS AND PLUGGING ON THE SWIRL VANES OF THE ATOMIZER DUE TO IMPROPER PARTICLE SIZING. ADDITIONAL PROBLEMS HAVE BEEN ENCOUNTERED WITH SOLIDS REMOVAL FROM THE BOTTOM OF THE SPRAY DRYER. THE SYSTEM WAS DESIGNED PRIMARILY TO REMOVE A FLY-ASH TYPE MATERIAL. THE UTILITY PLANS TO INSTALL A GRANULATOR IN THE BOTTOM OF THE SPRAY DRYER TO AID BYPRODUCT REMOVAL.

7/83 SYSTEM 744 8/83 SYSTEM 744 9/83 SYSTEM 720

# ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT BOTH PERFORMANCE AND CONTRACT AGREEMENT TESTING WAS PERFORMED IN MID-SEPTEMBER. NO CONCLUSIONS ARE YET AVAILABLE FOR RELEASE, BUT INITIAL RESULTS LOOK FAVORABLE.

INSTALLATION OF THE GRANULATOR FOR WASTE REMOVAL IS REPORTED NEAR COMPLETION. THE UTILITY NOW AWAITS THE DELIVERY OF THE REMAINING EQUIPMENT AND

MARQUETTE BOARD OF LIGHT & PWR: SHIRAS 3 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

MATERIALS TO COMPLETE THE JOB. ISOLATION OF THE DRYER HAS ENABLED THE UTILITY TO KEEP THE UNIT ON LINE DURING THE ENTIRE INSTALLATION PERIOD.

PROBLEMS WITH SCRUBBER MATERIAL BUILDUP ON THE SPRAY DRYER WALLS AND ATOM-IZER SWIRL VANES WAS DETERMINED TO BE A RESULT OF OPERATING THE SYSTEM NEAR OR BELOW THE DEW POINT TEMPERATURE. THE PROBLEM HAS BEEN RESOLVED BY ADDING INSTRUMENTATION WHICH ALLOWS THE OPERATORS TO MONITOR MORE CLOSELY THE INLET AND OUTLET TEMPERATURE OF THE SPRAY DRYER.

 10/83
 SYSTEM
 744

 11/83
 SYSTEM
 720

 12/83
 SYSTEM
 744

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURING THE FOURTH QUARTER OF 1983.

FINAL INSTALLATION AND TESTING OF THE NEW GRANULATOR WASTE REMOVAL SYSTEM IS SCHEDULED FOR FEBRUARY 1984.

GE ENVIRONMENTAL SERVICES, IN COOPERATION WITH THE UTILITY, WILL DESIGN AND TEST A NEW VARIABLE SPEED TYPE ATOMIZER AT THE SHIRAS 3 FACILITY. ATOMIZER SPEEDS WILL BE CONTROLLED VIA A DC MOTOR IN COMPARISON TO CONVENTIONAL DRIVE SYSTEMS, WHICH REQUIRE MANUALLY CHANGING THE DRIVE SHAFT PULLEY. PRESENTLY, A FULL DAY IS REQUIRED TO CHANGE A DRIVE SHAFT PULLEY.

1/84	SYSTEM	744
2/84	SYSTEM	696
3/84	SYSTEM	744
4/84	SYSTEM	720
5/84	SYSTEM	744
<b>6</b> /84	SYSTEM	720
7/84	SYSTEM	744
8/84	SYSTEM	744
9/84	SYSTEM	720

### ** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE FIRST THREE QUARTERS OF 1984.

# SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COMPANY NAME PLANT NAME	MICHIGAN SO CENTRAL PWR AGENCY PROJECT
UNIT NUMBER	1
CITY	LITCHFIELD
STATE	MICHIGAN
REGULATORY CLASSIFICATION	В
PARTICULATE EMISSION LIMITATION - NG/J	13. ( .030 LB/MMBTU)
SO2 EMISSION LIMITATION - NG/J	365 ( 850 LB/MMRTII)
NOX EMISSION LIMITATION - NG/J	365. ( .850 LB/MMBTU) ****** (****** LB/MMBTU)
NET PLANT GENERATING CAPACITY - MW	55
GROSS UNIT GENERATING CAPACITY MW	55
	50
NET UNIT GENERATING CAPACITY W/FGD - MW	= -
NET UNIT GENERATING CAPACITY WO/FGD - MW	51
EQUIVALENT SCRUBBED CAPACITY - MW	55
** UNIT DATA - BOILER AND STACK	
BOILER SUPPLIER	BABCOCK & WILCOX
BOILER TYPE	PULVERIZED COAL
BOILER SERVICE LOAD	BASE
DESIGN BOILER FLUE GAS FLOW - CU.M/S	
BOILER FLUE GAS TEMPERATURE - C	103.83 ( 220015 ACFM) 156.7 ( 314 F)
STACK HEIGHT - M	76. (250 FT)
STACK SHELL	CARBON STEEL
STACK TOP DIAMETER - M	2.9 ( 9.5 FT)
STACK TOP DIAMETER - IT	2.7 ( 7.3 11)
** FUEL DATA	
FUEL TYPE	COAL
FUEL GRADE	BITUMINOUS
AVERAGE HEAT CONTENT - J/G	28377. ( 12200 BTU/LB)
RANGE HEAT CONTENT - BTU/LB	11000-13000
	10.00
PANGE ASH CONTENT - Z	6.0-15.0
AVERAGE MOISTURE CONTENT - %	6.00
RANGE MOISTURE CONTENT - %	4.0-8.0
AVERAGE SULFUR CONTENT - %	2.25
RANGE SULFUR CONTENT - %	0.0-4.3
AVERAGE CHLORIDE CONTENT - %	*****
RANGE CHLORIDE CONTENT %	*****
*** PARTICLE CONTROL	
TARTICLE CONTROL	
** ESP	
NUMBER	1
TYPE	HOT SIDE
SUPPLIER	BELCO
INLET FLUE GAS CAPACITY - CU.M/S	126.2 ( 267510 ACFM)
INLET FLUE GAS TEMPERATURE - C	156.7 ( 314 F)
PRESSURE DROP - KPA	.1 ( 1. IN-H2O)
PARTICLE REMOVAL EFFICENCY - %	99.8
XX DARTICLE CONUMER	
** PARTICLE SCRUBBER	0
NUMBER	NONE
GENERIC TYPE	N/A
SPECIFIC TYPE	N/A
TRADE NAME/COMMON NAME	N/A
SHELL GENERIC MATERIAL	N/A
SHELL SPECIFIC MATERIAL	
LINER GENERIC MATERIAL	N/A
LINER SPECIFIC MATERIAL	N/A
GAS CONTACTING DEVICE TYPE	N/A
*** FGD SYSTEM	
XX CENERAL BATA	
** GENERAL DATA	THROWAWAY PRODUCT
SALEABLE PRODUCT/THROWAWAY PRODUCT	WET SCRUBBING
SO2 REMOVAL MODE	LIMESTONE
PROCESS TYPE	MAG
PROCESS ADDITIVES	BABCOCK & WILCOX
SYSTEM SUPPLIER	Process & Wicon

MICHIGAN SO CENTRAL PWR AGENCY: PROJECT 1 (CONT.)

```
CAMPBELL DEBOE & ASSOCIATES
   A-F FTRM
                                               FULL SCALE
   DEVELOPMENT LEVEL
   NEW/RETROEIT
                                               NEW
   UNIT DESIGN SOZ REMOVAL EFFICIENCY - %
                                                  90.00
                                                   1.8
   ENERGY CONSUMPTION - %
                                                1
   CURRENT STATUS
                                                5/83
   COMMERCIAL START-UP
                                                5/83
    INITIAL START-UP
   CONTRACT AWARDED
                                                6/79
** DESIGN AND OPERATING PARAMETERS
** QUENCHER/PRESATURATOR
   CONSTRUCTION MATERIAL GENERIC TYPE
                                               ND
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               ND
** ABSORBER
                                                1
   NUMBER
    NUMBER OF SPARES
                                                n
    GENERIC TYPE
                                               SPRAY TOWER
                                               OPEN COUNTERCURRENT SPRAY
    SPECIFIC TYPE
    TRADE NAME/COMMON TYPE
                                               N/A
                                               BABCOCK & WILCOX
    SUPPLIER
    DIMENSIONS - FT
                                               22.5 X 92.5
    SHELL GENERIC MATERIAL
                                               STAINLESS STEEL
    SHELL SPECIFIC MATERIAL
                                               AUSTENITIC
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                               TYPE 316L
    LINER GENERIC MATERIAL
                                               NONE
    LINER SPECIFIC MATERIAL
                                               N/A
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                               N/A
    GAS CONTACTING DEVICE TYPE
                                               NONE
    L/G RATIO - L/CU.M
                                                  1.3
                                                              ( 10.0 GAL/1000 ACF)
                                                              ( 7.9 FT/S)
( 186147 ACFM)
    SUPERFICAL GAS VELOCITY - M/SEC
                                                   2.4
    INLET GAS FLOW - CU. M/S
                                                  87.84
    INLET GAS TEMPERATURE - C
                                                 160.0
                                                              ( 320 F)
    SO2 REMOVAL EFFICIENCY - %
                                                  90.0
** MIST ELIMINATOR
    PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                               PRIMARY COLLECTOR
    NUMBER PER SYSTEM
                                                1
    GENERIC TYPE
                                               NR
    SPECIFIC TYPE
                                               ND
    TRADE NAME/COMMON TYPE
                                               NP
    CONFIGURATION
                                               VERTICAL
    NUMBER OF STAGES
                                                   2
    NUMBER OF PASSES PER STAGE
                                                   1
    DISTANCE BETWEEN STAGES - CM
                                                  25.91
                                                              (10.2 IN)
    DISTANCE BETWEEN VANES - CM
                                                   6.9
                                                               ( 2.70 IN)
    VANE ANGLES - DEGREES
                                                107
    PRESSURE DROP KPA
                                                               ( .3 IN-H20)
                                                    .1
    SUPERFICAL GAS VELOCITY - M/S
                                                   2.7
                                                               ( 8.8 FT/S)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               ORGANIC
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               FIBER-REINFORCED POLYESTER
    WASH WATER SOURCE
                                               BLENDED
    WASH RATE - L/S
                                                   5.4
                                                               ( 85 GAL/MIN)
** REHEATER
   NUMBER
    GENERIC TYPE
                                                IN-LINE
    SPECIFIC TYPE
                                                STEAM
    TRADE NAME/COMMON TYPE
                                                NR
    TEMPERATURE INCREASE - C
                                                              ( 50 F)
    INLET FLUE GAS FLOH RATE - CU. M/S
                                                 88.35
                                                              ( 187219 ACFM)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                               STAINLESS STEEL
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               AUSTENITIC
** FANS
   DESIGN
                                                NR
    FUNCTION
                                                NR
    AFPLICATION
                                                NR
    SERVICE
                                                NR
```

### MICHIGAN SO CENTRAL PWR AGENCY: PROJECT 1 (CONT.)

CONSTRUCTION MATERIAL GENERIC TYPE . NR

** DAMPERS

FUNCTION NR
GENERIC TYPE NR
SPECIFIC TYPE NR
CONSTRUCTION MATERIAL GENERIC TYPE NR
CONSTRUCTION MATERIAL SPECIFIC TYPE NR
LINER GENERIC MATERIAL TYPE NR
LINER SPECIFIC MATERIAL TYPE NR

** DUCTWORK

LOCATION HORIZONTAL IN-VERTICAL OUT
SHELL GENERIC MATERIAL TYPE STAINLESS STEEL
SHELL SPECIFIC MATERIAL TYPE AUSTENITIC
LINER GENERIC MATERIAL TYPE NR
LINER SPECIFIC MATERIAL TYPE NR

** REAGENT PREPARATION EQUIPMENT

FUNCTION WET BALL MILL
DEVICE NR
DEVICE TYPE NR

** TANKS

SERVICE NUMBER

ABSORBER RECYCLE
THICKENER OVERFLOW
SPARGER/OXIDIZER
REAGENT PREP PRODUCT
THICKENER UNDERFLOW
1

** PUMPS

NUMBER SERVICE LIME PRODUCT 2 SLURRY TRANSFER THICKENER UNDERFLOW 2 ABSORBER RECIRCULATION 3 2 SAND 2 CYCLONE 2 VACUUM FILTER FEED 2 FILTRATE 2 VACUUM CLARIFIED RECYCLE

** SOLIDS CONCENTRATING/DEWATERING

DEVICE THICKENER
NUMBER 1
NUMBER OF SPARES 0
CONFIGURATION CYLINDRICAL
DIMENSIONS - FT 70.0 DIA
FEED STREAM CHARACTERISTICS 17% SOLIDS
OUTLET STREAM CHARACTERISTICS 29% SOLIDS

** SOLIDS CONCENTRATING/DEWATERING

DEVICE VACUUM FILTER

NUMBER 2

NUMBER OF SPARES 1

SHELL SPECIFIC MATERIAL TYPE FIBER-REINFORCED POLYESTER
FEED STREAM CHARACTERISTICS 29% SOLIDS

OUTLET STREAM CHARACTERISTICS 60% SOLIDS

*** SLUDGE

** TREATMENT

METHOD FORCED OXIDATION

DEVICE NR

PROPRIETARY PROCESS NR

MICHIGAN SO CENTRAL PWR AGENCY: PROJECT 1 (CONT.)

** DISPOSAL

NATURE FINAL
TYPE LANDFILL
LOCATION OFF-SITE
SITE TRANSPORTATION METHOD TRUCK/RAIL
SITE TREATMENT NONE

** PROCESS CONTROL AND INSTRUMENTATION

CHEMICAL PARAMETERS PH-SOLIDS-ADDITIVES
MONITOR LOCATION RECYCLE SLURRY LINE
PROCESS CONTROL MANNER AUTOMATIC
PROCESS CHEMISTRY MODE FEEDBACK/FEED FORWARD

** WATER BALANCE

WATER LOOP TYPE

EVAPORATION WATER LOSS - LITER/S

SLUDGE HYDRATION WATER LOSS - LITER/S

POND SEEPAGE/RUNOFF WATER LOSS - LITER/S

CLOSED

4.0 (64 GPM)

1.1 (17 GPM)

RECEIVING WATER STREAM 105

MAKEUP WATER ADDITION - LITERS/S 5.4 ( 85 GPM)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

302 13013 10003 10003 10000

5/83 SYSTEM 744 6/83 SYSTEM 720

### ** PROBLEMS/SOLUTIONS/COMMENTS

INITIAL FGD OPERATIONS COMMENCED IN MAY 1983.

THE UTILITY REPORTED EXPERIENCING SOME MINOR PUMP BEARING AND VACUUM FILTER PROBLEMS DURING STARTUP.

7/83 SYSTEM 744 8/83 SYSTEM 744 9/83 SYSTEM 720

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED MINOR PROBLEMS ASSOCIATED WITH START-UP DURING THE THIRD QUARTER, HOWEVER, NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED.

 10/83
 SYSTEM
 744

 11/83
 SYSTEM
 720

 12/83
 SYSTEM
 744

### ** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE FOURTH QUARTER OF 1983.

 1/84
 SYSTEM
 744

 2/84
 SYSTEM
 696

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD RELATED OUTAGES WERE ENCOUNTERED DURING THE PERIOD OF OCTOBER 1983 THROUGH FEBRUARY 1984. SO2 REMOVAL DURING THIS PERIOD WAS ESTIMATED AT 95%.

MICHIGAN SO CENTRAL PWR AGENCY: PROJECT 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

THE LIMESTONE CRUSHER WAS REPLACED DURING THE PERIOD OF OCTOBER 1983 TO FEBRUARY 1984 DUE TO INADEQUATE SIZING.

THE UTILITY REPORTED PROBLEMS WITH THE VACUUM FILTRATION SYSTEM DURING THE PERIOD OF OCTOBER 1983 TO FEBRUARY 1984. THE PROBLEMS WERE SUBSEQUENTLY WORKED OUT AND REPAIRS WERE MADE.

3/84	SYSTEM	744
4/84	SYSTEM	720
5/84	SYSTEM	744
6/84	SYSTEM	720
7/84	SYSTEM	744
8/84	SYSTEM	744
9/84	SYSTEM	720

### ** PROBLEMS/SOLUTIONS/COMMENTS

A GENERATOR FAILURE OCCURRED IN LATE FEBRUARY 1984, FORCING A SHUT DOWN OF THE TOTAL FACILITY FOR THE REMAINDER OF THE FIRST THREE QUARTERS OF 1984.

THE UTILITY IS CURRENTLY DISCUSSING MODIFICATIONS OF THE DEWATERING SYSTEM TO PROVIDE EASIER AND MORE ECONOMICAL DEWATERING. A SIX MONTH TEST PROGRAM BEGINNING IN JANUARY 1985 WILL DETERMINE WHETHER OR NOT THE MODIFICATIONS SHOULD BE MADE PERMANENT.

### SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

MINNESOTA POWER & LIGHT COMPANY NAME CLAY BOSWELL PLANT NAME 4 UNIT NUMBER COHASSET CTTY MINNESOTA STATE REGULATORY CLASSIFICATION REGULATORY CLASSIFICATION

PARTICULATE EMISSION LIMITATION - NG/J

SO2 EMISSION LIMITATION - NG/J

NOX EMISSION LIMITATION - NG/J

NET PLANT GENERATING CAPACITY - MW

GROSS UNIT GENERATING CAPACITY - MW

554 GROSS UNIT GENERATING CAPACITY - MW
NET UNIT GENERATING CAPACITY W/FGD - MW
NET UNIT GENERATING CAPACITY WO/FGD - MW
EQUIVALENT SCRUBBED CAPACITY - ME 504 511 475 ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER COMBUSTION ENGINEERING BOILER TYPE PULVERIZED COAL BOILER SERVICE LOAD BASE DESIGN BOILER FLUE GAS FLOW - CU.M/S 1086.40 (2302181 ACFM)
BOILER FLUE GAS TEMPERATURE - C 148.9 (300 F)
STACK HEIGHT - M 183. (600 FT)
STACK SHELL CONCRETE 11.3 ( 37.0 FT) STACK TOP DIAMETER - M ** FUEL DATA FUEL TYPE COAL SUBBITUMINOUS FUEL GRADE AVERAGE HEAT CONTENT - J/G 19276. ( 8287 BTU/LB) RANGE HEAT CONTENT - BTU/LB 7509-9923 AVERAGE ASH CONTENT - % 9.40 RANGE ASH CONTENT - % ***** AVERAGE MOISTURE CONTENT - % 24.50 20.3-28.3 RANGE MOISTURE CONTENT - % AVERAGE SULFUR CONTENT - % .94 RANGE SULFUR CONTENT - % 0.4-2.8 [PACKMAKERS] AVERAGE CHLORIDE CONTENT - % .01 RANGE CHLORIDE CONTENT - % *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER TYPE NONE ** ESP NUMBER NUMBER OF SPARES n TYPE HOT SIDE WESTERN PREC. DIVISION, JOY INLET FLUE GAS CAPACITY - CU.M/S
INLET FLUE GAS TEMPERATURE - C 94.4 ( 200000 ACFM) 398.9 ( 750 F) .6 ( 3. IN-H20) PRESSURE DROP - KPA .6 99.7 PARTICLE REMOVAL EFFICENCY - % ** PARTICLE SCRUBBER

# NUMBER 4 NUMBER OF SPARES 1 GENERIC TYPE VENTURI TOWER SPECIFIC TYPE VARIABLE-THROAT/ADJUSTABLE DRUM TRADE NAME/COMMON NAME RADIAL FLOW VENTURI SUPPLIER PEABODY PROCESS SYSTEMS DIMENSIONS - FT 30.0 DIA X 40.0 SHELL GENERIC MATERIAL STAINLESS STEEL SHELL SPECIFIC MATERIAL AUSTENITIC LINER GENERIC MATERIAL ORGANIC LINER SPECIFIC MATERIAL GAS CONTACTING DEVICE TYPE NATURAL RUBBER NOHE NUMBER OF CONTACTING ZONES 1

### MINNESOTA POWER & LIGHT: CLAY BOSWELL 4 (CONT.)

```
841.7 (13360 GPM)
   LIQUID RECIRCULATION RATE - LITER/S
   L/G RATIO - LITER/CU.M
                                                 2.1
                                                             (16.0 GAL/1000ACF)
   PH CONTROL ADDITIVE
                                               ABSORBER SLURRY
   PRESSURE DROP KPA
                                                 3.0 (12.0 IN-H20)
    INLET GAS FLOW RATE - CU.M/S
                                                 394.4
                                                             ( 835840 ACFM)
    INLET GAS TEMPERATURE - C
                                               148.9
                                                            ( 300 F)
    PARTICLE REMOVAL EFFICIENCY - 2
                                                 99.7
*** FGD SYSTEM
** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                              THROWAWAY PRODUCT
    SO2 REMOVAL MODE
                                              WET SCRUBBING
    PROCESS TYPE
                                               LIME/ALKALINE FLYASH
    PROCESS ADDITIVES
                                               NONE
    SYSTEM SUPPLIER
                                               PEABODY PROCESS SYSTEMS
    A-E FIRM
                                               FRASCO
    DEVELOPMENT LEVEL
                                               FULL SCALE
    NEW/RETROFIT
                                              NEW
    UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.73
    UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                 89.00
    ENERGY CONSUMPTION - %
                                                 1.3
    CURRENT STATUS
                                                1
    COMMERCIAL START-UP
                                                4/80
    INITIAL START-UP
                                                2/80
 ** DESIGN AND OPERATING PARAMETERS
    DESIGN COAL SULFER CONTENT - %
                                                 2.80
                                            2.80
19980.3
    DESIGN COAL HEAT CONTENT J/G
                                                             ( 8590 BTU/LB)
    DESIGN COAL ASH CONTENT - %
                                               9.40
    DESIGN MOISTURE CONTENT - %
                                                  25.00
    DESIGN CHLORIDE CONTENT - %
                                                  .01
    SPACE REQUIREMENTS - SQ M
                                              14864.0
                                                             ( 160000 SQ FT)
    OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                               100.0
 ** QUENCHER/PRESATURATOR
    NUMBER
                                                0
 ** ABSORBER
    NUMBER
                                                4
    NUMBER OF SPARES
                                               1
    GENERIC TYPE
                                               SPRAY TOWER
                                              OPEN COUNTERCURRENT SPRAY
    SPECIFIC TYPE
    TRADE NAME/COMMON TYPE
                                              N/A
                                              PEABODY PROCESS SYSTEMS
    SUPPLIER
                                               35.0 DIA X 60.0
    DIMENSIONS - FT
                                              CARBON STEEL
    SHELL GENERIC MATERIAL
    SHELL SPECIFIC MATERIAL
                                              AISI 1110
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                             N/A
                                              ORGANIC
    LINER GENERIC MATERIAL
                                              NATURAL RUBBER
    LINER SPECIFIC MATERIAL
    LINER MATERIAL TRADE NAME/COMMON TYPE GAS CONTACTING DEVICE TYPE
                                              BLACK NATURAL RUBBER
                                              NONE
    NUMBER OF CONTACTING ZONES
                                               1
                                                            (33400 GPM)
( 52.2 GAL/1000 ACF)
(20.0 IN-H20)
                                                2104.
    LIQUID RECIRCULATION RATE - LITER/S
    L/G RATIO - L/CU.M
                                               7.0
5.0
    GAS-SIDE PRESSURE DROP - KPA
    SUFERFICAL GAS VELOCITY - M/SEC
                                                  3.7
                                                            ( 12.0 FT/S)
                                                             ( 640130 ACFM)
                                               302.08
    INLET GAS FLOW - CU. M/S
                                                             ( 128 F)
    INLET GAS TEMPERATURE - C
                                                 53.3
    SO2 REMOVAL EFFICIENCY - X
                                                  89.0
** MIST ELIMINATOR
    PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                               PRECOLLECTOR
    NUMBER PER SYSTEM
                                                4
    NUMBER OF SPARES PER SYSTEM
                                               1
    NUMBER PER MODULE
                                              BULK SEPARATION
    GENERIC TYPE
    SPECIFIC TYPE
                                               PERFORATED TRAYS
                                              SIEVE TRAY
    TRADE NAME/COMMON TYPE
                                              HORIZONTAL
    CONFIGURATION
```

# MINNESOTA POWER & LIGHT: CLAY BOSWELL 4 (CONT.)

LINER SPECIFIC MATERIAL TYPE

```
1
   NUMBER OF STAGES
   NUMBER OF PASSES PER STAGE
                                                    . 2
   PRESSURE DROP - KPA
                                                               ( 1.0 IN-H20)
   SUPERFICAL GAS VELOCITY - M/S
                                                    3.4
                                                               ( 11.0 FT/S)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                                STAINLESS STEEL
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                AUSTENITIC
                                                MAKEUP OVERSPRAY AND MAKEUP/SUPERNATANT MIXTURE
   WASH WATER SOURCE
   WASH RATE - L/S
                                                   29.9
                                                              ( 474 GAL/MIN)
** REHEATER
   MIMBER
                                                7
   GENERIC TYPE
                                                BYPASS
                                               HOT SIDE
   SPECIFIC TYPE
   TRADE NAME/COMMON TYPE
                                                N/A
                                                   5.0
   PERCENT GAS BYPASSED - AVG
    TEMPERATURE INCREASE - C
                                                   14.4
                                                                  26 F)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                               HIGH ALLOY
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               NICKEL BASE/CHROMIUM-IRON-MOLYBDENUM
** FANS
   NUMBER
                                                 4
   NUMBER OF SPARES
   DESIGN
                                                CENTRIFUGAL
   SUPPLIER
                                                GREEN FAN
   FUNCTION
                                               UNIT
   APPLICATION
                                                INDUCED DRAFT
    SERVICE
                                               WET
   FLUE GAS FLOW RATE - CU.M/S
                                                 320.33
                                                               ( 678800 ACFM)
    FLUE GAS TEMPERATURE - C
                                                  62.2
                                                               ( 144 F)
   CONSTRUCTION MATERIAL GENERIC TYPE
                                               HIGH ALLOY
** DAMPERS
   NUMBER
   FUNCTION
                                                ИD
   GENERIC TYPE
                                               GUILLOTINE
   SPECIFIC TYPE
                                               ΝR
   CONSTRUCTION MATERIAL GENERIC TYPE
                                                CARBON STEEL
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                AISI 1110
   LINER GENERIC MATERIAL TYPE
   LINER SPECIFIC MATERIAL TYPE
                                               NR
** DAMPERS
   NUMBER
   FUNCTION
                                                NΒ
   GENERIC TYPE
                                                GUILLOTINE
   SPECIFIC TYPE
                                               NR
   CONSTRUCTION MATERIAL GENERIC TYPE
                                               HIGH ALLOY
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                               NICKEL BASE/CHROMIUM-IRON-COPPER-MOLYBDENUM
   LINER GENERIC MATERIAL TYPE
                                                NR
   LINER SPECIFIC MATERIAL TYPE
                                               NR
** DAMPERS
   NUMBER
                                                 4
   FUNCTION
                                                NR
   GENERIC TYPE
                                                LOUVER
   SPECIFIC TYPE
                                               ИR
   CONSTRUCTION MATERIAL GENERIC TYPE
                                               CARBON STEEL
   CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                AISI 1110
   LINER GENERIC MATERIAL TYPE
                                               NΒ
   LINER SPECIFIC MATERIAL TYPE
                                               ИR
** DUCTWORK
   LOCATION
                                                ABSORBER TO REHEATER
   DIMENSIONS
                                               12.0 DIA
    SHELL GENERIC MATERIAL TYPE
                                               CARBON STEEL
    SHELL SPECIFIC MATERIAL TYPE
                                               AISI 1110
    LINER GENERIC MATERIAL TYPE
                                               ORGANIC
```

GLASS FLAKE-FILLED POLYESTER

### MINNESOTA POWER & LIGHT: CLAY BOSWELL 4 (CONT.)

```
** DUCTWORK
   LOCATION
                                                REHEAT SECTION
   DIMENSIONS
    SHELL GENERIC MATERIAL TYPE
                                                STAINLESS STEEL
    SHELL SPECIFIC MATERIAL TYPE
                                                AUSTENITIC
    LINER GENERIC MATERIAL TYPE
                                                NONE
    LINER SPECIFIC MATERIAL TYPE
                                                N/A
** REAGENT PREPARATION EQUIPMENT
   FUNCTION
                                                SLAKER
   DEVICE
                                                NR
   DEVICE TYPE
                                                ΝR
   MANUFACTURER
                                                PEABODY PROCESS SYSTEMS
   NUMBER
   FULL LOAD DRY FEED CAPACITY - M.TONS/HR
                                                   18.2
                                                                ( 20 TPH)
   PRODUCT QUALITY - % SOLIDS
                                                   20.0
** TANKS
   SERVICE
                                                NUMBER
                                                -----
    ABSORBER RECYCLE
                                                   4
    REAGENT PREP PRODUCT
                                                   1
    MIST ELIMINATOR WASH
                                                   1
   FLYASH
                                                   1
** PUMPS
                                                NUMBER
    SERVICE
    -----
                                                 -----
    ALKALI FEED
                                                   2
    FLY ASH SLURRY FEED
                                                   2
    SCRUBBER RECIRCULATION
                                                   8
    ABSORBER RECIRCULATION
                                                  12
    WASH WATER
** SOLIDS CONCENTRATING/DEWATERING.
                                                NONE
    DEVICE
*** SLUDGE
                                                              ( 21.7 TPH)
    FULL LOAD SLUDGE QUANTITY - M.TONS/HR (DRY)
                                                   19.7
    MOISTURE CONTENT - % TOTAL FREE WATER
                                                   45.0
    % CASO3 - DRY
                                                     5.0
                                                     3.0
    % CASO4 DRY
    % CAOH2 DRY
% CACO3 - DRY
                                                     . 0
                                                     1.0
                                                    91.0
    % ASH - DRY
** TREATMENT
                                                BLEED
    METHOD
                                                N/A
    DEVICE
                                                N/A
    PROPRIETARY PROCESS
** DISPOSAL
                                                 FINAL
    NATURE
                                                 POND
    TYPE
                                                OFF-SITE
    LOCATION
                                                PIPELINE
    SITE TRANSPORTATION METHOD
    SITE TREATMENT
                                                CLAY LINING
                                                 276 ACRES
    SITE DIMENSIONS
                                                              ( 7814.0 ACRE-FT)
    SITE CAPACITY - CU.M
                                                   9556522
                                                  35
    SITE SERVICE LIFE - YRS
** PROCESS CONTROL AND INSTRUMENTATION
                                                 PH AND SO2
    CHEMICAL PARAMETERS
                                                 DENSITY IN RECYCLE TANK
    PHYSICAL VARIABLES
                                                 PH 3-6; 7-9% SOLIDS
    CONTROL LEVELS
                                                 DUPONT AND LEAR SIEGLER FOR SO2
    MONITOR TYPE
                                                RECYCLE TANK
    MONITOR LOCATION
                                                AUTOMATIC
    PROCESS CONTROL MANNER
```

MINNESOTA POWER & LIGHT: CLAY BOSWELL 4 (CONT.)

PROCESS CHEMISTRY MODE FEEDBACK

** WATER BALANCE

CLOSED

WATER LOOP TYPE
EVAPORATION WATER LOSS - LITER/S
SLUDGE HYDRATION WATER LOSS - LITER/S
SLUDGE INTERSTITIAL WATER LOSS - LITERS/S
MAKEUP WATER ADDITION - LITERS/S
SOURCE OF MAKEUP WATER

27.6 ( 438 GPM) .1 ( 1 GPM) 4.3 ( 69 GPM) 32.0 ( 508 GPM) RIVER WATER

** CHEMICALS AND CONSUMPTION

FUNCTION

NAME

PRINCIPAL CONSTITUENT

CONSUMPTION

POINT OF ADDITION

** FGD SPARE CAPACITY INDICES

SCRUBBER - %

ABSORBER - %

ABSORBER - %

33.0

33.0

** FGD SPARE COMPONENT INDICES

SCRUBBER 1.0

ABSORBER 1.0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

4/80 SYSTEM

6/80 SYSTEM

** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER BEGAN OPERATIONS ON FEBRUARY 26, 1980 AND FIRED OIL THROUGH THE MONTH OF MARCH. INITIAL FGD SYSTEM OPERATIONS BEGAN IN EARLY APRIL WITH THE BOILER FIRING COAL FOR TESTING PURPOSES. THE UNIT WAS SHUTDOWN IN MID-APRIL TO RECTIFY MINOR SHAKEDOWN PROBLEMS. A TRIAL RUN OF THE FGD SYSTEM IN AN INTEGRATED MODE OCCURRED IN LATE APRIL.

720

720

5/80 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

SHAKEDOWN OPERATIONS CONTINUED THROUGH THE SECOND QUARTER OF 1980. THE FGD SYSTEM WILL BE FINE TUNED TO MEET DESIGN CRITERIA THROUGH JULY. TO DATE THE UTILITY REPORTED THAT, ALTHOUGH MANY TYPICAL STARTUP PROBLEMS ATTRIBUTABLE TO OPERATOR ERROR AS WELL AS MECHANICAL MALFUNCTIONS HAVE OCCURRED, NO UNUSUAL PROBLEMS HAVE OCCURRED. THE COMPLIANCE TEST IS SCHEDULED FOR EARLY SEPTEMBER.

7/80	1	87.8	100.0	86.8				
	2	97.8	100.0	96.7				
	3	100.0	100.0	100.0				
	4	.0		. 0				
	SYSTEM	96.1	100.0	95.0	720	712	684	79.0
8/80	1	71.8	100.0	62.9				
	2	75.5	100.0	66.1				
	3	29.4	100.0	25.8				
	4	49.7	100.0	43.5				
	SYSTEM	75 <b>.5</b>	100.0	66.1	744	652	492	61.7
9/80	1	71.6	100.0	71.0				
	2	89.6	100.0	88.7				
	3	14.7	100.0	14.5				

PERIOD	MODULE AVA	AILABILI	TY OPERABILITY	RELIABILITY	UTILIZATION	SO2 PART.				
	4		65.1	100.0	64.5					
	SYSTEM		80.3	100.0	79.6		744	737	592	73.7
	** PROBLE	15/SOLUT	IONS/COMMENTS							
			THE FGD SYSTER				OPERAT	TION.	MUCH O	THE
10/80	1		31.6	100.0	22.6					
	2		38.4	100.0	27.4					
	3		.0		. 0					
	4			100.0	59.7					
	SYSTEM		51.2	100.0	36.6		744	531	272	59.1
	** PROBLE	15/ <b>5</b> 0LUT	IONS/COMMENTS							
			THE UTILITY R			E HOURS AND	UNAVA	LABLE	HOURS (	DURING
			THE UNIT OUTA	GE TIME WAS	DUE TO MISCEL	LANEOUS MAII	NTENANO	CE AND	AN INS	PEC-
11/80	1	94.4	67.2	100.0	60.7					
11,00	2	85.6	55.5	100.0	50.1					
	3	98.1	59.1	100.0	53.3					
	4	55.4	26.0	100.0	23.4					
	SYSTEM	100.0	69.2	100.0	62.5		720	650	450	60.8
	** PROBLE	MS/SOLUT	IONS/COMMENTS							
			MODULE 4 OUTA GENERAL REPAI		ING NOVEMBER N	IAS DUE TO N	ECESSAI	RY CLEA	NING A	<b>4</b> D
12/80	1	100.0	100.0	100.0	100.0					
	2	93.4		100.0 100.0	61.3					
	3	19.4		100.0	2.4					
	4	96.5	87.6	100.0	86.6					
	SYSTEM	100.0	87.6	100.0	83.5		744	73 <b>5</b>	621	89.7
	** PROBLE	MS/SOLUT	TIONS/COMMENTS							
			DURING DECEMB REPAIRS TO TH			NAS DUE TO G	ENERAL	MAINTE	NANCE	DHA
1/81	1	100.0	100.0	100.0	100.0					
	2	69.4	48.1	100.0	48.1					
	3	100.0	98.4	100.0	98.4					
	4	73.1	38.7	100.0	38.7					
	SYSTEM	100.0	95.0	100.0	95.0		744	744	707	93.0
2/81	1	100.0	92.2	100.0	91.5					
	2	82.1	36.4	100.0	36.2					
	3	75.7	48.9	100.0	48.5					
	4	100.0	67.8	100.0	67.3		/ 70		F/ F	0/ 0
	SYSTEM	100.0	81.7	100.0	81.1		672	667	545	86.0
3/81	1	79.8	55.6	100.0	53.2					
	2	40.2	29.5	100.0	28.2					
	3	100.0	94.8	100.0	90.7					
	,	100.0	95.8	100.0	91.7					
	4 SYSTEM	100.0	91.8	100.0	87.9		744	712	/ - /	88.9

MINNESOTA POWER & LIGHT: CLAY BOSWELL 4 (CONT.)

-----PERFORMANCE DATA------PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS FACTOR ** PROBLEMS/SOLUTIONS/COMMENTS DURING THE FIRST QUARTER 1981 THE UTILITY REPORTED THAT NO MAJOR FGD-RELAT-ED PROBLEMS WERE ENCOUNTERED. 4/81 1 54.3 28.2 100.0 26.3 70.5 2 88.1 100.0 65.7 94.0 56.7 100.0 3 52.8 88.1 100.0 100.0 82.1 100.0 81.1 100.0 75.6 720 671 545 83.5 SYSTEM 5/81 1 95.2 51.2 100.0 46.8 100.0 95.3 75.2 67.7 2 3 98.0 66.0 100.0 59.5 4 . 0 . 0 .0 SYSTEM 96.1 64.3 100.0 58.0 744 671 432 63.4 ** PROBLEMS/SOLUTIONS/COMMENTS DURING MAY MODULE 4 WAS DOWN FOR AN INSPECTION, MAINTENANCE AND VENTURI MODIFICATIONS. 6/81 1 100.0 71.6 100.0 71.6 74.9 2 96.1 74.9 100.0 100.0 3 94.0 78.3 78.3 33.5 31.7 100.0 31.7 SYSTEM 100.0 85.5 100.0 720 720 616 89.5 85.5 ** PROBLEMS/SOLUTIONS/COMMENTS THE UTILITY REPORTED THAT NO MAJOR PROBLEMS WERE ENCOUNTERED DURING THE MONTH OF JUNE. 7/81 1 66.5 56.2 100.0 49.2 2 100.0 93.9 100.0 82.1 3 100.0 78.8 100.0 69.0 79.0 29.5 100.0 25.8 SYSTEM 100.0 86.1 100.0 75.4 744 651 561 78.0 8/81 1 27.3 9.3 100.0 8.3 100.0 100.0 2 100.0 91.5 3 78.5 31.3 100.0 28.0 4 100.0 100.0 100.0 91.5 SYSTEM 100.0 80.2 100.0 73.1 744 665 544 73.8 9/81 100.0 1 60.0 100.0 56.8 2 100.0 100.0 100.0 95.4 3 58.2 41.8 100.0 39.6 66.7 65.0 100.0 61.5 SYSTEM 100.0 88.9 100.0 84.4 720 682 608 87.8 ** PROBLEMS/SOLUTIONS/COMMENTS THERE WERE NO MAJOR FGD-RELATED PROBLEMS REPORTED FOR THE THIRD QUARTER 10/81 1 100.0 90.8 100.0 90.8 2 56.4 56.4 100.0 56.4 3 87.6 78.5 100.0 78.5 60.7 58.7 100.0 58.7 SYSTEM 100.0 94.8 100.0 744 744 705 88.0 94.8

51.2

100.0

11/81 1

87.5

67.6

MINNESOTA POWER & LIGHT: CLAY BOSWELL 4 (CONT.)

PERIOD	MODULE	AVAILABILITY	OPERABILITY	PERFORMAN	UTILIZATION		PER			
	2	35.0		100.0	29.4					
	3	100.0	38.8 100.0	100.0	76.4					
	4	64.4	80.6		61.1					
	SYSTEM	93.8	95.9	100.0	72.8		720	546	524	66.5
12/81	1	100.0	77.4	100.0	77.4					
	2	100.0	98.0	100.0						
	3	25.0	20.2	100.0	20.2					
	4 EVETEM	75.8 100.0	75.1	100.0 100.0	75.1 90.2		7//	<b>-</b>		70 /
	2121511	100.0	90.2	100.0	90.2		744	/44	671	79.6
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS							
				EPORTED THAT URTH QUARTER		D-RELATED PR	OBLEMS	WERE E	NCOUNTI	ERED
1/82	1	78.0	48.0 100.0	100.0 100.0	48.0					
	2	100.0	100.0		100.0					
	3	75.1	75.1 82.5	100.0	75.1					
	4 SYSTEM	90.4 100.0	82.5 100.0	100.0	82.5 100.0		744	744	744	98.0
							, , , ,	, , , ,		,0.0
2/82		.0	.0 100.0	100.0	.0 97.8					
	2 3	100.0	89.6	100.0	81.8					
	4		100.0		94.0					
	SYSTEM	100.0	100.0 99.8	100.0 100.0	91.2		672	614	613	86.0
3/82	1	68.4	59.5	100.0	59.0					
	2	100.0	92.3 94.6	100.0 100.0	91.5					
	3	100.0		100.0	53.5					
	4 SYSTEM	47.8 100.0	43.8 96.7	100.0 100.0	43.4 96.0		744	738	714	92.0
				,00.0	70.0		, , , ,	750	7.2.4	,
	** PRO	BLEMS/SOLUTIO -		EDODTED THAT	NO MAJOD PRI	ODIEMO MEDE	ENCOLIN	TENEN N	UDTNC:	TUE
			IRST QUARTER	EPORTED THAT	NU MAJUR PRI	UBLENS WERE	ENCUUN	ונאבט ט	OKING	INC
4/82	SYSTEM						720			
5/82	SYSTEM						744			
6/82	1	64.9	65.4	100.0	50.4					
	2	100.0	86.7	100.0	66.8					
	3	83.9	62.2	100.0	47.9					
	4	82.4	82.2	100.0	63.3 76.2		720	555	549	62.9
	SYSTEM	100.0	98.8	100.0	76.2		720	333	347	02.7
	** PRO	BLEMS/SOLUTIO _		EPORTED THAT	. NO MA 100 EC	D DELATED DD	OB! EME	Nene e	NCO! BIT	EDED
			URING JUNE.	EPURIED THAT	NO ROCK FG	D-RELATED PR	OBLENS	MEKE E	,14000141	LKLD
7/82	SYSTEM						744			
8/82	SYSTEM						744			
9/82	SYSTEM						720			
10/82	SYSTEM						744			
	SYSTEM						720			
-1/02	3131611									

MINNESOTA POWER & LIGHT: CLAY BOSWELL 4 (CONT.)

******				PERFORMAN	CE DATA						
PERIOD			OPERABILITY		UTILIZATION	% REN	10VAL	PER	BOILER	FGD	CAP.
				<b></b>					HOURS		FACTOR
12/82	SYSTEM							744			
1/83	SYSTEM							744			
2/83	SYSTEM							672			
3/83	SYSTEM							744			
	** PROS	BLEMS/SOLUTIO	NS/COMMENTS								
		<b>T</b>	NFORMATION WA	AC INJAVATIADI	E EOD THE DE	בפדחם מ	)E 1111	V 1092	THEOLIC	J MADCI	1 1007
		4	INFORMATION A	43 UNAVAILABI	LE FOR THE PE	ERIOD (	JF 30L	1 1702	Inkoodi	THARCE	1 1703.
4/83	1	96.9	80.3	100.0							
	2	76.0	50.6 66.1 33.5	100.0	50.6						
	3	65.3	66.1	100.0	66.0						
	4	34.9	33.5	100.0	33.5						
	SYSTEM	91.0	76.8	100.0	76 <b>.7</b>			720	719	553	82.0
5/83	1	78.2	59.4 65.2	100.0	59.4						
	2	88.6	65.2	100.0	65.2						
	3	79.2	15.2	100.0	15.2						
	4	96.6	15.2 93.5	100.0	93.5						
		100.0	77.8	100.0	77.8			744	744	579	68 9
	01012				,,,,				, , , ,	3,,	00.7
6/83	1	89.7	56.8 1.8	100.0	35.3						
	2	71 0	1 8	100.0	1.1						
	3	99.4	53.9	100.0							
	4	77.0	23.7	100.0	33. <b>3</b>						
		86.8	37.5	100.0	23.3			720	448	168	34.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
		т	THE UTILITY RE	EDODTED THAT	NO MATOR EC	1_BE! AT	ren <del>on</del>	001 EMC	HEDE EI		DED
			OURING THE PER					OBLEMS	MERE EI	4Ċ00I411	LKED
		_				12 270.	•				
7/83	1	96.8	78.1	100.0	69.6						
	2	100.0	19.8	100.0	17.6						
	3	100.0	72.5	100.0 100.0	46.7						
	4	100.0	97.7	100.0	74.7						
	SYSTEM	100.0	83.7 84.7	100.0				744		F/ 0	70.0
	3131211	100.0	04.7	100.0	75.5			744	663	502	78.0
8/83	1	100.0	33.5	100.0	33.5						
	2	98.3			85.9						
	3	100.0									
	4	86.0									
	SYSTEM		67.9	100.0	67.9			_,,	<b></b>		70 5
	313141	100.0	89.2	100.0	89.2			744	744	664	78.5
9/83	1	100.0	55.9	100 0	44.0						
,, 03	2			100.0	44.8						
	3	100.0	79.0	100.0	63.3						
		100.0	72.5	100.0	58.1						
	4	92.2	50.5	100.0	40.4						
	SYSTEM	100.0	86.0	100.0	68.8			720	577	496	61.0
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS								
		1	THE UTILITY R	EPORTED THAT	NO MAJOR FG	D-RELA	TED PR	OBLEMS	WERE E	нсоинт	ERED
		C	DURING THE PE	RIOD OF JULY	THROUGH SEP	TEMBER	1983.				
10/83	1	98.1	9.0	100.0	4.5						
	2	100.1	100.0	100.0	53.1						
	3	100.1	59.6								
	4	100.1		100.0	29.7						
	SYSTEM		96.2	100.0	47.9						
	SISIEM	100.0	88.3	100.0	45.1			744	371	335	34.2

744

744

720

7/84 SYSTEM

8/84 SYSTEM

9/84 SYSTEM

		**				ON % REMOVAL SO2 PART.				
<del>-</del>					_					
11/83		60.0	.0		.0					
	2	100.0	51.0	100.0	51.0					
	3	100.0	63.8	100.0	63.8					
	4	100.0	79.9	100.0	79.9					
	SYSTEM	100.0	64.9	100.0	64.9		720	720	467	62.8
12/83		89.8	9.9	100.0	9.9					
	2	100.0	30.4	100.0	30.4					
	3	100.0	52.4	100.0	52.4					
	4	100.0	45.6	100.0	45.6					
	SYSTEM	100.0	46.1	100.0	46.1		744	744	343	88.0
	** PROB	LEMS/SOLUTION	NS/COMMENTS							
		TI	HE UTILITY R	EPORTED THAT	NO MAJOR	FGD-RELATED PR	OBLEMS	WERE E	NCOUNTI	ERED
		ום	JRING THE FO	URTH QUARTER	OF 1983.					
1/84	1	40.2	25.9	100.0	22.2					
	2	100.0	100.0	100.0 100.0	93.8					
	3	68.8	71.0	100.0	61.0					
	4	100.0	100.0	100.0	89.4					
	SYSTEM		99.0	100.0	88.8		744	639	661	80.0
2/84	1	100.0	86.5		86.4					
	2	54.0	46.6	100.0	46.6					
	3	83.0	66.8	100.0	66.7					
	4	100.0	97.1	100.0	96.9					
	SYSTEM	100.0			98.9		696	695	688	85.0
3/84	1	61.0	48.2	100.0	47.8					
	2	99.6	98.0	100.0	97.3					
	3	100.0	00 /	100.0	98.7					
	4	77.2	47.1	100.0	46.8					
	SYSTEM		97.5		96.9		744	739	721	97.0
4/84	1	100.0	80.9	100.0	80.7					
	2	100.0	80.9 84.2	100.0	80.7 84.0					
	3	100.0	38.2	100.0	38.1					
	4	95.8	85.5	100.0	85.3					
		100.0			96.0		720	718	691	94.4
5/84	1	43.1	36.4	100.0	36.1					
	2	100.0	100.0	100.0	99.4					
	3	90.3	69.8	100.0	69.2					
	4	100.0	98.4	100.0	97.6					
	SYSTEM	100.0	100.0	100.0	100.0		744	738	744	97.0
	SISIEM	100.0	100.0	100.0	100.0		, , , ,	, 30	, , , ,	,,. <b>.</b>
6/84	1	100.0	92.3	100.0	92.3 30.5					
	2	34.5	30.5	100.0						
	3	100.0	92.1	100.0	92.1					
	4	76.7	56.9	100.0	56.9		74-	700	/ 50	00.0
	SYSTEM	100.0	90.6	100.0	90.6		720	720	652	90.2
	** PROB	LEMS/SOLUTIO	NS/COMMENTS							
			HE UTILITY R							

UTILITY FGD SURVEY: OCTOBER 1983 - SEPTEMBER 1984
MINNESOTA POWER & LIGHT: CLAY BOSWELL 4 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE THIRD QUARTER OF 1984.

# SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COMPANY NAME MINNKOTA POWER PLANT NAME MILTON R. YOUNG UNIT NUMBER 2 CENTER CITY NORTH DAKOTA STATE REGULATORY CLASSIFICATION PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW GROSS UNIT GENERATING CAPACITY - MW NET UNIT GENERATING CAPACITY W/FGD - MW
NET UNIT GENERATING CAPACITY WO/FGD - MW 402 409 374 EQUIVALENT SCRUBBED CAPACITY - MW ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER BABCOCK & WILCOX BOILER TYPE CYCLONE BOILER SERVICE LOAD BASE 958.33 (2030800 ACFM) 176.7 (350 F) 168. (550 FT) CONCRETE DESIGN BOILER FLUE GAS FLOW - CU.M/S BOILER FLUE GAS TEMPERATURE - C STACK HEIGHT - M STACK SHELL ( 25.0 FT) 7.6 STACK TOP DIAMETER - M ** FUEL DATA FUEL TYPE COAL LIGNITE FUEL GRADE 15119. ( 6500 BTU/LB) AVERAGE HEAT CONTENT - J/G RANGE HEAT CONTENT - BTU/LB 6000-6800 AVERAGE ASH CONTENT - % 8.90 7.2-14.3 RANGE ASH CONTENT - % 38.00 AVERAGE MOISTURE CONTENT - % RANGE MOISTURE CONTENT - % 30-45 AVERAGE SULFUR CONTENT - % .4-.8 RANGE SULFUR CONTENT - % ****** AVERAGE CHLORIDE CONTENT - % ***** RANGE CHLORIDE CONTENT - % *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER 0 NONE TYPE ** FABRIC FILTER NUMBER ** ESP 2 NUMBER NUMBER OF SPARES COLD SIDE TYPE WHEELABRATOR-FRYE SUPPLIER 479.2 (1015400 ACFM) 176.7 ( 350 F) .3 ( 1. IN-H20) INLET FLUE GAS CAPACITY - CU.M/S INLET FLUE GAS CAPACITY - CU.M/S
INLET FLUE GAS TEMPERATURE - C .3 99.8 PRESSURE DROP - KPA PARTICLE REMOVAL EFFICENCY - % ** PARTICLE SCRUBBER Ω NUMBER NONE GENERIC TYPE N/A SPECIFIC TYPE N/A TRADE NAME/COMMON NAME SHELL GENERIC MATERIAL N/A N/A SHELL SPECIFIC MATERIAL LINER GENERIC MATERIAL N/A LINER SPECIFIC MATERIAL N/A

N/A

GAS CONTACTING DEVICE TYPE

### *** FGD SYSTEM

```
** GENERAL DATA
                                               THROWAWAY PRODUCT
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                               WET SCRUBBING
    SO2 REMOVAL MODE
                                               LIME/ALKALINE FLYASH
   PROCESS TYPE
   PROCESS ADDITIVES
                                               NONE
   SYSTEM SUPPLIER
                                               THYSSEN/CEA
                                               SANDERSON & PORTER
    A-E FIRM
   DEVELOPMENT LEVEL
                                               FULL SCALE
   NEW/RETROFIT
                                              NEW
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.60
                                                  78.00
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
    ENERGY CONSUMPTION - %
                                                   1.6
    CURRENT STATUS
                                                1
    COMMERCIAL START-UP
                                                6/78
    INITIAL START-UP
                                                9/77
    CONTRACT AWARDED
                                                4/75
** DESIGN AND OPERATING PARAMETERS
    OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                92 ft
** QUENCHER/PRESATURATOR
   NUMBER
                                                0
** ABSORBER
   NUMBER
                                                2
   NUMBER OF SPARES
                                                1
    GENERIC TYPE
                                               SPRAY TOWER
   SFECIFIC TYPE
                                               OPEN COUNTERCURRENT SPRAY
    TRADE NAME/COMMON TYPE
                                              N/A
    SUPPLIER
                                               THYSSEN/CEA
    DIMENSIONS - FT
                                               40.0 DIA X 120.0
    SHELL GENERIC MATERIAL
                                              CARBON STEEL
    SHELL SPECIFIC MATERIAL
                                               AISI 1110
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                              N/A
    LINER GENERIC MATERIAL
                                               ORGANIC
    LINER SPECIFIC MATERIAL
                                               GLASS FLAKE-FILLED POLYESTER
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                               FLAKELINE 500
    GAS CONTACTING DEVICE TYPE
                                               NONE
   NUMBER OF CONTACTING ZONES
    LIQUID RECIRCULATION RATE - LITER/S
                                                3456.
                                                             (54850 GPM)
    L/G RATIO - L/CU.M
                                                8.7
                                                             ( 64.8 GAL/1000 ACF)
    GAS-SIDE PRESSURE DROP - KPA
                                                   . 2
                                                             ( 1.0 IN-H20)
    SUPERFICAL GAS VELOCITY - M/SEC
                                                             ( 9.1 FT/S)
                                                  2.8
    INLET GAS FLOW - CU. M/S
                                                             ( 847000 ACFM)
                                                399.70
    INLET GAS TEMPERATURE - C
                                                168.3
                                                             ( 335 F)
    SO2 REMOVAL EFFICIENCY - %
                                                  85.0
    PARTICLE REMOVAL EFFICENCY - %
                                                  70.0
** MIST ELIMINATOR
   PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                               PRIMARY COLLECTOR
    NUMBER PER SYSTEM
                                                2
   NUMBER OF SPARES PER SYSTEM
                                                1
   NUMBER PER MODULE
                                                1
   GENERIC TYPE
                                               IMPINGEMENT
    SPECIFIC TYPE
                                              BAFFLE
    TRADE NAME/COMMON TYPE
                                              CLOSED VANE
    CONFIGURATION
                                              HORIZONTAL
   NUMBER OF STAGES
                                                   1
    NUMBER OF PASSES PER STAGE
                                                   5
    FREEBOARD DISTANCE - M
                                                   2.44
                                                              (8.0 FT)
    VANE ANGLES - DEGREES
                                                120
    PRESSURE DROP - KPA
                                                   . 2
                                                              ( 1.0 IN-H20)
    SUPERFICAL GAS VELOCITY - M/S
                                                   2.8
                                                              ( 9.1 FT/S)
    CONSTRUCTION MATERIAL GENERIC TYPE
                                              ORGANIC
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              POLYPHENYLENE
   WASH WATER SOURCE
                                               BLENDED
    WASH FREQUENCY
                                               CONTINUOUS
   WASH RATE - L/S
                                                            ( 800 GAL/MIN)
                                                 50.5
```

** REHEATER  NUMBER  NUMBER OF SPARES  GENERIC TYPE  SPECIFIC TYPE  TRADE NAME/COMMON TYPE  LOCATION  PERCENT GAS BYPASSED - AVG  TEMPERATURE INCREASE - C  INLET FLUE GAS TEMPERATURE - C  OUTLET FLUE GAS TEMPERATURE - C  NUMBER OF TUBES PER BUNDLE  CONSTRUCTION MATERIAL GENERIC TYPE  CONSTRUCTION MATERIAL SPECIFIC TYPE	1 0 BYPASS COLD SIDE N/A OUTLET DUCT 12.0 22.2 ( 40 F) 54.4 ( 130 F) 76.7 ( 170 F) 0 CARBON STEEL AISI 1110
** FANS NUMBER NUMBER OF SPARES DESIGN SUPPLIER FUNCTION APPLICATION SERVICE FLUE GAS FLOW RATE - CU.M/S FLUE GAS TEMPERATURE - C PRESSURE DROP - KPA CONSTRUCTION MATERIAL GENERIC TYPE	2 1 AXIAL BUFFALO FORGE UNIT FORCED DRAFT DRY 519.09 (1100000 ACFM) 176.7 ( 350 F) 3.2 (10.6 IN-H20) CARBON STEEL
** FANS NUMBER NUMBER OF SPARES DESIGN SUPPLIER FUNCTION APPLICATION SERVICE PRESSURE DROP - KPA CONSTRUCTION MATERIAL GENERIC TYPE	2 1 AXIAL TLT-BABCOCK BOOSTER FORCED DRAFT DRY 8.8 (28.8 IN-H20) CARBON STEEL
** DAMPERS  GENERIC TYPE  SPECIFIC TYPE  CONSTRUCTION MATERIAL GENERIC TYPE  CONSTRUCTION MATERIAL SPECIFIC TYPE  LINER GENERIC MATERIAL TYPE  LINER SPECIFIC MATERIAL TYPE	GUILLOTINE NR CARBON STEEL AISI 1110 NONE N/A
** DAMPERS  GENERIC TYPE  SPECIFIC TYPE  CONSTRUCTION MATERIAL GENERIC TYPE  CONSTRUCTION MATERIAL SPECIFIC TYPE  LINER GENERIC MATERIAL TYPE  LINER SPECIFIC MATERIAL TYPE	GUILLOTINE NR STAINLESS STEEL AUSTENITIC NOME N/A
** DAMPERS  GENERIC TYPE  SPECIFIC TYPE  CONSTRUCTION MATERIAL GENERIC TYPE  CONSTRUCTION MATERIAL SPECIFIC TYPE  LINER GENERIC MATERIAL TYPE  LINER SPECIFIC MATERIAL TYPE	LOUVER NR CARBON STEEL AISI 1110 NONE N/A
** DAMPERS  GENERIC TYPE  SPECIFIC TYPE  CONSTRUCTION MATERIAL GENERIC TYPE  CONSTRUCTION MATERIAL SPECIFIC TYPE  LINER GENERIC MATERIAL TYPE  LINER SPECIFIC MATERIAL TYPE	BUTTERFLY NR STAINLESS STEEL AUSTENITIC NONE N/A

MINNKOTA POWER: MILTON R. YOUNG 2 (CONT.)

** DUCTWORK  LOCATION  SHELL GENERIC MATERIAL TYPE  SHELL SPECIFIC MATERIAL TYPE  LINER GENERIC MATERIAL TYPE  LINER SPECIFIC MATERIAL TYPE	INLET CARBON STEEL AISI 1110 NONE N/A
** DUCTWORK LOCATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	OUTLET CARBON STEEL AÎSI 1110 ORGANIC GLASS FLAKE-FILLED POLYESTER
** DUCTWORK  LOCATION  SHELL GENERIC MATERIAL TYPE  SHELL SPECIFIC MATERIAL TYPE  LINER GENERIC HATERIAL TYPE  LINER SPECIFIC MATERIAL TYPE	BYPASS CARBON STEEL AISI 1110 NONE N/A
** REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE DEVICE TYPE MANUFACTURER NUMBER NUMBER NUMBER OF SPARES FULL LOAD DRY FEED CAPACITY - M.TONS/HR PRODUCT QUALITY - % SOLIDS	SLAKER NR NR WALLACE & TIERNAN 1 0 3.6 ( 4 TPH) 13.0
** TANKS  SERVICE  ABSORBER RECYCLE  THICKENER UNDERFLOW  FLY ASH SLURRY FEED  LIME SLAKER TRANSFER  THICKENER OVERFLOW  CLARIFIER OVERFLOW/ME WASH  TRAY RECYCLE  LIME SLURRY FEED	NUMBER  2 1 1 1 1 2 1 1
** PUMPS  SERVICE  ABSORBER RECIRCULATION  TRAY RECIRCULATION  TRAY SPRAY/CLARIFIER OVERFLOW  THICKENER UNDERFLOW  LIME SLAKER TRANSFER  LIME SLURRY FEED  FLYASH SLURRY FEED  MIST ELIMINATOR SPRAY  CLARIFIER UNDERFLOW  FILTER BELT WASH  BLOW DOWN SUMP	NUMBER
** SOLIDS CONCENTRATING/DEWATERING DEVICE NUMBER	CENTRIFUGE 2
** SOLIDS CONCENTRATING/DEWATERING DEVICE NUMBER DIMENSIONS - FT CAPACITY SHELL GENERIC MATERIAL TYPE	THICKENER 2 130 DIA X 15 HIGH 3000000 INORGANIC

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MINNKOTA POWER: MILTON R. YOUNG 2 (CONT.)
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SHELL SPECIFIC MATERIAL TYPE CONCRETE LINER GENERIC MATERIAL TYPE ORGANIC LINER SPECIFIC MATERIAL TYPE FIBER-REINFORCED POLYESTER ABSORBER BLEED FEED STREAM SOURCE FEED STREAM CHARACTERISTICS 12% SOLIDS 40% SOLIDS OUTLET STREAM CHARACTERISTICS OUTLET STREAM DISPOSITION TO VACUUM FILTER TO FLYASH SLURRY, VACUUM FILTER WASH, & ME WASH OVERFLOW STREAM DISPOSITION

### ** SOLIDS CONCENTRATING/DEWATERING

DEVICE VACUUM FILTER NUMBER 2 NUMBER OF SPARES n 750 TON/DAY CAPACITY CARBON STEEL SHELL GENERIC MATERIAL TYPE AISI 1110 SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE ORGANIC NATURAL RUBBER LINER SPECIFIC MATERIAL TYPE BELT GENERIC MATERIAL TYPE ORGANIC THICKENER & CLARIFIER UNDERFLOW
30% SOLIDS
60% SOLIDS BELT SPECIFIC MATERIAL TYPE FEED STREAM SOURCE FEED STREAM CHARACTERISTICS OUTLET STREAM CHARACTERISTICS OUTLET STREAM DISPOSITION TO LANDFILL OVERFLOW STREAM DISPOSITION TO THICKENER

### *** SLUDGE

FULL LOAD SLUDGE QUANTITY - M.TONS/HR (DRY) 19.1 ( 21.0 TPH)
MOISTURE CONTENT - % TOTAL FREE WATER 40.0
% CASO3 - DRY .0

### ** TREATMENT

METHOD DEWATERED
DEVICE N/A
PROPRIETARY PROCESS N/A

### ** DISPOSAL

NATURE FINAL
TYPE LANDFILL
LOCATION OFF-SITE
SITE TRANSPORTATION METHOD TRUCK
SITE TREATMENT CLAY LINING

### ** DISPOSAL

NATURE INTERIM
TYPE POND
LOCATION ON-SITE
SITE TRANSPORTATION METHOD PIPELINE
SITE TREATMENT CLAY LINING
SITE SERVICE LIFE - YRS 1

### ** DISPOSAL

NATURE INTERIM

TYPE POND

LOCATION ON-SITE

SITE DIMENSIONS 11.92 ACRES X 15 FT DEEP [SEMI-CIRCLE]

SITE CAPACITY - CU.M 218672 ( 178.8 ACRE-FT)

### ** DISPOSAL

NATURE
TYPE
LOCATION
SITE DIMENSIONS
SITE CAPACITY - CU.M

### ** PROCESS CONTROL AND INSTRUMENTATION

CHEMICAL PARAMETERS
PHYSICAL VARIABLES
CONTROL LEVELS

POND ON-SITE

INTERIM

11.92 ACRES X 15 FT DEEP [SEMI-CIRCLE] 218672 ( 178.8 ACRE-FT)

### PH

PERCENT SOLIDS

SOLIDS 5.5-12%; PH 4.0-5.5

MINNKOTA POWER: MILTON R. YOUNG 2 (CONT.)

PROCESS CONTROL MANNER MANUAL

** WATER BALANCE

WATER LOOP TYPE CLOSED

EVAPORATION WATER LOSS - LITER/S 34.6 (550 GPM)
MAKEUP WATER ADDITION - LITERS/S 44.1 (700 GPM)

** CHEMICALS AND CONSUMPTION

FUNCTION ABSORBENT
NAME FLY ASH
PRINCIPAL CONSTITUENT 20-25% CAO, 5-9% MGO
CONSUMPTION 16 TPH

UTILIZATION - % 83.0
POINT OF ADDITION SLURRY FEED TANK

** FGD SPARE CAPACITY INDICES

ABSORBER - % 100.0

** FGD SPARE COMPONENT INDICES

ABSORBER 1.0

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

### 0/77 SYSTEM

### ** PROBLEMS/SOLUTIONS/COMMENTS

ALTHOUGH THE MILTON R YOUNG 2 SCRUBBING SYSTEM ORIGINAL DESIGN DID NOT INCLUDE SPARE FGD CAPACITY, THE SYSTEM DOES, IN ACTUALITY, GENERALLY HAVE A SPARE MODULE AS A CONSEQUENCE OF THE VARIABILITY IN LIGNITE SULFUR CONTENT. THE LIGNITE BLEND AT M.R.YOUNG 2 VARIES IN SULFUR CONTENT FROM 0.35 TO 1.3%. WHEN THE SULFUR CONTENT RISES TO 1.3% BOTH SCRUBBING TOWERS ARE REQUIRED (WITH 5 TO 15% OF THE FLUE GAS BYPASSED FOR REHEAT). WHEN THE SULFUR CONTENT DROPS TO 0.7% OR BELOW ONLY ONE TOWER IS REQUIRED. 0.7% SULFUR IS TYPICAL FOR THE M.R.YOUNG 2 LIGNITE BLEND. BECAUSE OF THE EFFECTIVE SPARE MODULE THE SYSTEM DEPENDABILITY FIGURES THAT APPEAR IN THIS SECTION WILL GENERALLY NOT BE EQUIVALENT TO THE AVERAGE OF THE MODULAR DEPENDABILITIES (E.G. WITH 0.7% SULFUR LIGNITE THERE IS 100% SPARE CAPACITY. IF A-MODULE OPERATES THE FIRST HALF OF THE MONTH (50%) AND B-MODULE THE SECOND HALF OF THE MONTH (50%) THE TOTAL SYSTEM UTILIZATION WILL BE 100%).

9/77 SYSTEM 720

### ** PROBLEMS/SOLUTIONS/COMMENTS

INITIAL SCRUBBING OPERATIONS BEGAN IN SEPTEMBER. THE FGD SYSTEM IS EXPECTED TO BE OPERATING IN AN INTEGRATED MODE IN LATE OCTOBER, HOWEVER, A SCRUBBER LINING FAILURE MAY RESULT IN SOME DELAYS. THE UTILITY EXPECTS THE SYSTEM OPERATIONS TO STABILIZE BY MID-NOVEMBER.

10/77 SYSTEM 744

11/77 SYSTEM 720

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED INTERMITTENT FGD SYSTEM OPERATIONS SINCE START-UP.

MAJOR OPERATIONAL PROBLEMS HAVE OCCURRED AS A RESULT OF SEVERE WINTER WEATHER CONDITIONS, PARTICULARLY NUMEROUS INSTANCES OF FROZEN AND RUPTURED LINES. THE SYSTEM WAS SHUT DOWN DURING THE FIRST PART OF THE MONTH OF DECEMBER TO INSTALL HEAT TRACING IN THE LIQUID CIRCUIT.

SOME MINOR PROBLEMS HAVE OCCURRED WITH THE FLOW METERS (ROTAMETERS).

THE UTILITY ENCOUNTERED PROBLEMS WITH GUILLOTINE GAS DAMPER GUIDES DURING

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART, HOURS HOURS FACTOR

OCTOBER AND NOVEMBER.

12/77 SYSTEM 744

### ** PROBLEMS/SOLUTIONS/COMMENTS

THERE WAS AN EMERGENCY SHUTDOWN ON DECEMBER 5 AS A RESULT OF TURBINE BEARING DAMAGE. THE SHUTDOWN CONTINUED SO THAT A COMPLETE TURBINE INSPECTION COULD BE MADE.

WORK CONTINUED ON INSTALLATION OF ELECTRICAL HEAT TRACING ON SLURRY LINES AND WATER PIPING.

1/78 SYSTEM 744

### ** PROBLEMS/SOLUTIONS/COMMENTS

BECAUSE OF THE TURBINE BEARING PROBLEMS THE COMPLIANCE TEST ORIGINALLY SCHEDULED FOR THE DECEMBER-JANUARY PERIOD WAS TENTATIVELY RESCHEDULED WITH THE EPA FOR THE END OF MARCH. THE UTILITY EXPECTS THE FGD SYSTEM TO ACHIEVE EQUILIBRIUM (WATER BALANCE) WHEN THE UNIT COMES BACK ON LINE IN FEBRUARY.

2/78 SYSTEM 672

#### ** PROBLEMS/SOLUTIONS/COMMENTS

BOTH THE BOILER AND FGD SYSTEM CAME BACK ON LINE FEBRUARY 21 AFTER COM-PLETION OF THE TURBINE REPAIRS. THE COMPLIANCE TEST HAS AGAIN BEEN RE-SCHEDULED WITH EPA FOR THE END OF MAY.

ONE FORCED-DRAFT FAN (UPSTREAM OF THE FGD SYSTEM) HAD AN OIL LEAK AND A SHAFT ALIGNMENT PROBLEM. THE FAN WAS TAKEN OFF LINE AND SHIPPED TO BUFFALO FORGE FOR REPAIRS.

THE VACUUM FILTER MALFUNCTIONED, ALLOWING LARGER SIZE PARTICLES TO ESCAPE THE FILTER. THIS CAUSED THE RUBBER LINING DOWN STREAM TO PEEL WHICH, IN TURN, CREATED A PLUGGING PROBLEM. EIMCO ENGINEERS ARE PRESENTLY STUDYING THE PROBLEM AND HOPE TO INCORPORATE MODIFICATIONS TO IMPROVE THE PERFOR-MANCE OF THE FILTERS.

3/78 SYSTEM 744

4/78 SYSTEM 720

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE DAMAGED FD FAN WAS REINSTALLED DURING APRIL. THE AFFECTED MODULE WAS DOWN FROM FEBRUARY 23 THROUGH APRIL 10.

744 5/78 SYSTEM

720 6/78 SYSTEM

### ** PROBLEMS/SOLUTIONS/COMMENTS

COMPLIANCE TESTING TOOK PLACE DURING THE WEEK OF JUNE 5. THE REPORT SHOULD BE AVAILABLE TO THE UTILITY BY THE END OF JUNE.

THE UNIT WAS DOWN WITH DAMPER PROBLEMS (DOWN ON THE 24TH OF JUNE). AP-PARENTLY THE CHAINS THAT PULL THE GUILLOTINE DAMPERS WERE UNDERDESIGNED AND PRONE TO FAILURE. THE CHAINS ARE CURRENTLY BEING REPLACED.

744 7/78 SYSTEM

MINNKOTA POWER: MILTON R. YOUNG 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

8/78 SYSTEM 744

#### ** PROBLEMS/SOLUTIONS/COMMENTS

OFFICIAL RESULTS OF THE COMPLIANCE TEST PERFORMED ON JUNE 6 ARE STILL NOT AVAILABLE. BECAUSE OF INTERMITTENT OPERATION, FGD SYSTEM PERFORMANCE FIGURES ARE NOT YET AVAILABLE.

9/78 SYSTEM 720

10/78 SYSTEM 744

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE THICKENER HAS BEEN A MAJOR PROBLEM AREA. THE POLYETHYLENE LINER WAS ACCIDENTLY PIERCED WHILE REPAIRS WERE BEING MADE TO SOME OTHER COMPONENTS. THE LINER IS CURRENTLY BEING PATCHED.

THE UTILITY REPORTED THAT OPERATION OF THE BOILER AND FGD SYSTEM CONTINUED ON AN INTERMITTENT BASIS THROUGHOUT THE PERIOD.

11/78 SYSTEM 720

### ** PROBLEMS/SOLUTIONS/COMMENTS

THICKENER PROBLEMS ARE CONTINUING. THE RUBBER LINER HAS BEEN DETATCHING FROM THE THICKENER CONE. THE THICKENER MUST BE DRAINED TO MAKE THE REPAIRS.

FAN PROBLEMS OCCURRED DURING THE PERIOD. THERE IS NO DAMPER BETWEEN THE MODULE AND FAN. UNDER SOME OPERATING CONDITIONS WET GAS CAN BACK INTO THE FAN AREA RESULTING IN CORROSION AND OTHER MOISTURE RELATED PROBLEMS.

12/78 4.6 4.6 A 5.1 B 37.7 28.4 25.7 SYSTEM 42.3 33.5 33.8 30.3 744 673 225 54.0

### ** PROBLEMS/SOLUTIONS/COMMENTS

MINNKOTA POWER COOP REPORTED THE FOLLOWING STATISTICS FOR THE YEAR OF 1978:

TOTAL PERIOD HOURS: 8760
TOTAL BOILER HOURS: 6926
TOTAL A-MCDULE HOURS: 1790
TOTAL B-MODULE HOURS: 2110

ANNUAL BOILER CAPACITY FACTOR: 66.7%

FGD SYSTEM PERFORMANCE:

A-MODULE B-MODULE SYSTEM
AVAILABILITY 92.3 28.5 46.1
OPERABILITY 28.0 25.9 52.7
RELIABILITY 53.9
UTILIZATION 22.2 20.4 41.7

THE B-TOWER WAS OUT OF SERVICE DURING DECEMBER DUE TO PLUGGING OF THE THICKENER UNDERFLOW BY RUBBER LINING. THE THICKENER WAS PUMPED OUT AND REPAIRED.

1/79 Α 4.6 5.1 4.6 В 37.7 28.4 25.7 SYSTEM 42.3 33.5 33.8 30.3 744 225 54.0 673

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

### ** PROBLEMS/SOLUTIONS/COMMENTS

SOME WEATHER-RELATED PROBLEMS OCCURRED WITH FGD SYSTEM PIPING FREEZE-UPS.

THE UTILITY REPORTED THAT THE A-TOWER WAS OUT OF SERVICE FOR A PERIOD IN JANUARY DUE TO BROKEN INLET ISOLATION DAMPER CHAINS.

THE A-TOWER WAS OUT OF SERVICE TO REPAIR A BOOSTER FAN SERVO MECHANISM THROUGH JANUARY 28.

THE B-TOWER WAS OUT OF SERVICE FROM DECEMBER 27 THROUGH JANUARY 31 DUE TO A FAN MOTOR FAILURE.

THE UTILITY REPORTED THAT EROSION PROBLEMS IN THE SCRUBBER TOWERS ARE SEVERE ENOUGH THAT HOLES HAVE BEEN DISCOVERED IN TOWER WALLS.

2/79	A B System	19.4 32.1 51.5	26.5 44.0 70.5	70.5	19.4 32.1 51.5	672	491	346	58.1
3/79	A B SYSTEM	19.4 32.1 51.5	26.5 44.0 70.5	70.5	19.4 32.1 51.5	744	543	383	58.1

### ** PROBLEMS/SOLUTIONS/COMMENTS

TWO DAYS OF DOWN TIME WERE REQUIRED TO REMOVE LOOSE RUBBER FROM THE THICKENER PIPING DURING THE FEBRUARY-MARCH PERIOD.

A BOOSTER FAN MOTOR FIRE OCCURRED IN THE A-MODULE.

HOLES IN THE B-SIDE ABSORBER TOWER WERE REPAIRED DURING THE PERIOD.

COLD WEATHER INHIBITED SCRUBBER STARTUPS AFTER REPAIRS WERE MADE DURING THE PERIOD.

4/79	A B	3.0 57.1	3.2 61.6		3.0 57.1				
	SYSTEM	60.1	64.8	65.4	60.1	720	668	432	69.4
5/79	A	3.0	3.2		3.0				
	В	57.1	61.6		57.1				
	SYSTEM	60.1	64.8	65.4	60.1	744	690	448	88.4

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE A-MODULE IS STILL EXPERIENCING FAN PROBLEMS. DURING APRIL AND MAY THE FAN HAD ALIGNMENT PROBLEMS POSSIBLY RELATED TO THE FAN FOUNDATION.

DURING APRIL AND MAY HOLES WERE REPAIRED IN THE ABSORBER WALLS, VALVE REPAIRS WERE MADE, AND REPAIRS WERE MADE ON A THICKENER DRIVE GEAR.

6/79	A	17.2	17.2		17.2				
	В	36.3	36.3		36.3				
	SYSTEM	52.8	52.8	52.8	52.8	720	720	380	88.7

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE A-TOWER WAS DOWN FOR REPAIR TO THE FLAKE LINING.

THE FGD SYSTEM WAS DOWN FOR PART OF THE MONTH FOR REPAIRS AFTER EXCESS SOLIDS ENTERING THE TRAY RECYCLE LOOP OVERLOADED THE CLARIFIER.

MINNKOTA POWER: MILTON R. YOUNG 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

AN A-TOWER TRAY RECYCLE DISTRIBUTION HEADER WAS CLEANED DURING JUNE.

THE SYSTEM WAS FORCED OUT OF SERVICE WHEN BOILER PROBLEMS CAUSED AN EXCESSIVE AMOUNT OF HEAVY PARTICLES (SLAG CARRYOVER) TO ENTER THE FGD SYSTEM RESULTING IN THE PLUGGING OF SEVERAL LINES AND STOPPING THE THICKENER RAKE. SLUDGE HAD TO BE DREDGED AND HAULED OUT FROM THE TOP OF THE THICKENER.

THE A-TOWER WAS OUT OF SERVICE DUE TO PROBLEMS WITH THE WATER BALANCE AND THE VACUUM FILTERS AS WELL AS TO UNPLUG THE ABSORBER BLEED LINE. LIME WAS USED FOR SEVERAL DAYS AS MAKE UP CHEMICAL (AS OPPOSED TO PRIMARILY ALKALINE FLYASH) TO EASE THE HIGH SOLIDS PROBLEM.

A-TOWER AGITATOR GEARS WHICH FAILED AS A RESULT OF A CLARIFIER OVERLOAD WERE REPLACED DURING THE PERIOD.

7/79	A	44.5	44.5		44.5	
	В	.0	.0		.0	
	SYSTEM	44.0	44.0	44.0	44.0	

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY HAS REPORTED THAT A TRAY RECYCLE CONTROL VALVE AND AN ABSORBER TRAIN VALVE FAILED DURING JULY.

744 331 86.7

744

THE UTILITY REPORTED PROBLEMS WITH PLUGGING IN THE MIST ELIMINATORS, THE THICKENER AND IN THE ABSORBER FEED LINE.

THE UNIT EXPERIENCED A BOOSTER FAN TRIP IN JULY.

PROBLEMS WITH THE VACUUM FILTERS AND THE SEAL WATER PUMP WERE ENCOUNTERED.

THE ABSORBER AGITATOR WAS REPLACED DURING JULY.

8/79	A	28.7	28.7		28.7				
	В	10.6	10.6		10.6				
	SYSTEM	39.0	39.0	39.0	39.0	744	744	293	92.3

### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING AUGUST EXCESSIVE VIBRATION AND HIGH BEARING TEMPERATURE IN THE A-SIDE BOOSTER FAN WERE ENCOUNTERED CAUSING SOME DOWN TIME.

THE INABILITY TO ADD ALKALI (FLYASH OR LIME) TO THE SYSTEM CAUSED SOME OPERATIONAL PROBLEMS ON THE A-SIDE SCRUBBER.

DURING AUGUST THE B-SIDE THICKENER RAKE WAS BURIED IN THE SLUDGE. THE SLUDGE HAD TO BE REMOVED BY MINING IT FROM THE TOP.

PLUGGING OF THE FLYASH TANK AND THE LIME SLURRY FEED LINE CAUSED SOME B-SIDE OUTAGE TIME DURING AUGUST.

DUE TO A LACK OF LIME (THE UTILITY SUPPLY WAS EXHAUSTED) THE FGD SYSTEM HAD TO SHUT DOWN.

THE HOLES IN THE SIDES OF THE B-SIDE ABSORBER TOWER HAD TO BE REPAIRED CAUSING SOME OUTAGE TIME IN AUGUST.

9/79	A	21.4	21.5		21.4				
		1.2	1.2		1.2				
	SYSTEM	23.0	23.0	23.0	23.0	720	717	163	96.6

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING SEPTEMBER THE A-SIDE WAS DOWN DUE TO HEAVY SOLIDS IN THE THICKENER AND CLARIFIER. HIGH VIBRATIONS WERE EXPERIENCED WITH THE BOOSTER FAN.

THE B-SIDE REMAINED OUT OF SERVICE DUE TO PROBLEMS WITH THE THICKENER AND CLARIFIER.

10/79 A .0 .0 .0 B 31.3 31.4 31.3 SYSTEM 31.3 31.4 31.4 31.3

SYSTEM 31.3 31.4 31.4 31.3 744 743 233 89.7

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY IS IN THE PROCESS OF CLEANING THE CLARIFIER.

THE CLARIFIER AGITATOR DRIVE GEAR FAILED CAUSING DOWN TIME FOR REPAIR IN OCTOBER.

THE BLEED LINE TO THE THICKENER PLUGGED AND NEEDED MAINTENANCE.

THE GEAR HOUSING FAILED ON THE THICKENER LIFT MECHANISM CAUSING OUTAGE TIME FOR REPAIR.

11/79 .6 . 7 .6 15 4 16.7 15.4 В SYSTEM 17.4 16.0 17.4 16.0 720 661 115 80.0

### ** PROBLEMS/SOLUTIONS/COMMENTS

AN EXCESS OF SOLIDS CAUSED PLUGGING IN THE THICKENER AND THE CLARIFIER DURING NOVEMBER.

12/79 Α 26.6 31.5 26.6 9.7 11.5 9.7 SYSTEM 43.0 36.3 744 628 270 67.2 36.3 43.0

### ** PROBLEMS/SOLUTIONS/COMMENTS

PLUGGING OF THE SEAL WATER SYSTEM RESULTED IN SOME OUTAGE TIME DURING DECEMBER.

BOOSTER FAN PROBLEMS RELATED TO EXCESSIVE VIBRATION WERE ENCOUNTERED ON MODULE B IN DECEMBER.

A HOLE IN A BLOCKING VALVE RESULTED IN SOME DOWNTIME.

THE GEAR HOUSING FAILED ON THE THICKENER LIFT MECHANISM.

1/80 7.1 10.5 7.1 . 0 R . 0 ٠.0 7.1 504 53 58.5 SYSTEM 7.1 10.5 10.5 744

### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING JANUARY, COLD WEATHER CAUSED SOME PIPE LINES AND A BOOSTER FAN TO ICE UP.

A HIGH PERCENTAGE OF COARSE SOLIDS IN THE THICKENER CAUSED SOME OUTAGE TIME. THE WORM GEAR ON THE THICKENER FAILED ADDING TO THE OUTAGE TIME.

CLEANING AND REPAIR OF THE THICKENER WAS COMPLICATED BY SUB-ZERO AMBIENT TEMPERATURES.

MINNKOTA POWER: MILTON R. YOUNG 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

2/80 SYSTEM .0 .0 696 696 0 97.1

### ** PROBLEMS/SOLUTIONS/COMMENTS

PROBLEMS RELATED TO THE COLD WEATHER CONTINUED THROUGH FEBRUARY. ICE ON THE BOOSTER FAN HAD TO BE MELTED BEFORE IT COULD BE OPERATED.

SHAFT SLEEVES ON SEVERAL SPRAY RECYCLE PUMPS WERE REPLACED DURING FERRUARY.

THE GEAR REDUCER FAILED ON THE B-SIDE ABSORBER AGITATOR PREVENTING SCRUBBER OPERATION.

THE ISOLATION DAMPER CHAINS BROKE DURING THE MONTH.

3/80	A	22.6	22.6		22.6				
	В	6.2	6.2		6.2				
	SYSTEM	28.9	28.8	28.8	28.8	744	743	214	89.1

### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING MARCH COLD WEATHER CONTINUED TO BE A PROBLEM.

THE TORQUE SWITCHES ON THE ISOLATION DAMPERS WERE REPLACED. THE DAMPER PROBLEMS CAUSED THE BOOSTER FAN TO TRIP. THE OUTAGE TIME WAS EXTENDED BECAUSE THE UTILITY HAD TO WAIT FOR THE SWITCHES TO BE DELIVERED.

AN EXCESSIVE AMOUNT OF COARSE PARTICLES IN THE THICKENER CONTINUED TO BE A PROBLEM. PLUGGED BLEED LINES FROM THE ABSORBER TO THE THICKENER WERE ALSO ENCOUNTERED.

THE A-SIDE ABSORBER AGITATOR ANCHOR BOLTS SHEARED DURING MARCH CAUSING MODULE DOWN TIME.

THE SHAFT SLEEVES ON THE SPRAY RECYCLE PUMPS WOULD NOT HOLD THE PUMP GLAND PACKING. THE SHAFT SLEEVES ARE CURRENTLY BEING REPLACED.

4/80	A	100.0	.0		.0			
	В	.0	.0	.0	.0			
	SYSTEM	100.0	.0	.0	.0	720	154	0

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS DOWN FOR APPROXIMATELY 3 WEEKS FOR THE ANNUAL UNIT OUTAGE DURING APRIL.

PLUGGED BLEED LINES AND THE REPLACEMENT OF THE SHAFT SLEEVES ON THE RECYCLE PUMPS CAUSED THE FGD SYSTEM TO REMAIN OFF LINE DURING THE TIME THE BOILER OPERATED.

5/80	A	.0	. 0		. 0			
	В	47.2	48.4	50.6	45.6			
	SYSTEM	47.2	48.4	50.6	45.6	744	700	339

### ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE B WAS OPERATED DURING MAY WHILE REPAIR WORK WAS BEING DONE ON MODULE A.

THE REPAIRS ON MODULE A INCLUDED WORK ON THE SPRAY RECYCLE NOZZLE PIPING, AND THE RECYCLE HEADER.

THE VALVES ON BOTH THE SPRAY RECYCLE PUMP AND THE DISCHARGE SPRAY CYCLE

-----PERFORMANCE DATA------

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

SUE FART, HOURS HOURS HOURS ACTION

PUMP WERE REPAIRED.

THE ABSORBER LINING HAS STARTED TO WEAR AND IS NOW BEING REPAIRED.

HIGH SOLIDS RESULTED IN THICKNER LINE PLUGGING. HIGH SOLIDS ALSO CAUSED PROBLEMS WITH THE RAKE AND CONE. BOTH THE THICKNER AND THE CLARIFIER HAD TO BE DRAINED AND CLEANED.

THE ABSORBER AGITATOR TUNNEL WAS ALSO CLEANED DURING THE MONTH.

6/80 A .0 . 0 . 0 R 41.8 40.4 41.4 39.3 SYSTEM 41.8 40.4 41.4 39.3 720 701 283

#### ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE B CONTINUED TO OPERATE THROUGH JUNE.

PROBLEMS WITH THE THICKNER CONTINUED THROUGH THE MONTH. HIGH SOLIDS CAUSED PROBLEMS WITH THE RAKE MECHANISM AND THE LIMIT SWITCH.

TROUBLE WAS ENCOUNTERED DURING JUNE WITH THE VACUUM FILTER.

THE REPAIR WORK CONTINUED ON THE ABSORBER FLAKE LININGS.

MODULE A REPAIR WORK CONTINUED DURING JUNE.

7/8 <b>0</b>	A	.0	.0		.0				
	В	65.3	64.5	65.8	52.0				
	SYSTEM	65.3	64.5	65.8	52. <b>0</b>	744	600	387	60.0

### ** PROBLEMS/SOLUTIONS/COMMENTS

PROBLEMS WITH THE RAKE MECHANISM AND UNDERFLOW PUMPS IN THE THICKENER CONTINUED IN JULY. HIGH SOLIDS IN THE THICKENER ARE CAUSED WHEN FLY ASH IS ADDED TO THE LIME IN THE ABSORBER TOWER. THE ABSORBER REAGENT IS CHANGED TO STRAIGHT LIME WHEN THIS OCCURS.

PROBLEMS WERE ENCOUNTERED WITH THE TWO VACUUM FILTER PUMPS. ONE WAS BEING REBUILT WHILE THE OTHER FUNCTIONED POORLY.

REPAIRS WERE MADE TO THE LEAK IN THE ABSORBER TOWER.

PROBLEMS WERE REPORTED WITH THE MOTOR AND DISCHARGE VALVE ON THE TRAY RECYCLE PUMPS.

THE FGD SYSTEM WAS NOT PLACED IN SERVICE WHEN THE BOILER WAS RUN AT REDUCED LOAD DURING THE MONTH.

8/80	A	90.7	54.3	98.8	53.9				
	В	56.9	44.2	99.4	44.0				
	SYSTEM	99.2	98.6	99.2	98. <b>0</b>	744	739	729	92.8

### ** PROBLEMS/SOLUTIONS/COMMENTS

BOTH MODULES WERE OPERATED DURING AUGUST.

DURING THE MONTH, MAINTENANCE WORK WAS DONE ON THE SPRAY RECYCLE PUMPS (TEFLON PACKING), THE VACUUM FILTER DRUM, SPRAY NOZZLES, THE ABSORBER AGITATOR, THE CLARIFIER CONE, AND THE THICKNER RAKE MECHANISM.

9/80	A	70.1	72.6	100.0	66.9				
	В	66.7	25.1	100.0	23.2				
	SYSTEM	100.0	97.9	100.0	90.3	720	664	650	78.5

MINNKOTA POWER: MILTON R. YOUNG 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART, HOURS HOURS FACTOR

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE FGD SYSTEM WAS AVAILABLE DURING ALL OF SEPTEMBER.

BOTH MODULES WERE OPERATED DURING THE MONTH.

10/80	A	90.4	85.4	87.1	76.2				
	В	17.7	. 0		.0				
	SYSTEM	100.0	85.4	87.1	76.2	744	664	744	75.7

### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING OCTOBER AVAILABILITY FOR MODULE B WAS LOW DUE TO LEAKS IN THE TOWER.

11/80	A	42.2	40.4	100.0	38.7				
	В	98.6	54.0	96.4	50.1				
	SYSTEM	100.0	94.5	99.1	90.6	720	690	720	88.6

### ** PROBLEMS/SOLUTIONS/COMMENTS

AVAILABILITY WAS LOW FOR MODULE A DUE TO LEAKS IN THE TOWER DURING THE MONTH OF NOVEMBER.

12/80	A	41.5	33.2	54.5	40.0				
•	В	30.0	29.5	88.6	28.4				
	SYSTEM	71.5	62.8	66.7	60.5	744	716	450	92.4

### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING DECEMBER AVAILABILITY WAS LOW DUE TO DOWN TIME NECESSARY TO CONVERT FROM A THICKENER TO SLUDGE PONDS AND PROBLEMS WITH THE OVERFLOW LEVEL CONTROL OF THE ABSORBER.

ISOLATION DAMPER PROBLEMS DURING THE MONTH DELAYED THE STARTUP OF THE FGD SYSTEM.

1/81	A	83.8	94.4	100.0	83.9				
	В	. 0	.0		.0				
	SYSTEM	83.9	94.4	100.0	83.9	744	661	624	83.8

### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING JANUARY THE SYSTEM WAS SHUT DOWN FOR PART OF THE MONTH TO REPACK THE ABSORBER TOWER AGITATOR.

ADDITIONAL OUTAGE TIME WAS DUE TO ISOLATION DAMPER PROBLEMS.

2/81 A	33.9	11.8	100.0	11.8				
В	83.3	87.4	100.0	83.3				
SYSTEM	95.0	99.8	100.0	95.0	672	641	639	88.5

### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING FEBRUARY NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED.

3/81	A	58.3	66.3	100.0	58.3			
	В	29.6	28.4	100.0	25.0			
	SYSTEM	87.8	94.6	100.0	83.8	744	655	620 78.7

720

360

661

20 78.8

487 80.9

MINNKOTA POWER: MILTON R. YOUNG 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

\$02 PART. HOURS HOURS FACTOR

### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING MARCH SOME OUTAGE TIME WAS DUE TO ISOLATION DAMPER PROBLEMS.

BOOSTER FAN PROBLEMS CAUSED ADDITIONAL DOWN TIME.

4/81 A .0 .0 .0 .0 .0 B 2.7 5.4 5.6 2.7 SYSTEM 2.7 5.4 5.6 2.7

** PROBLEMS/SOLUTIONS/COMMENTS

DURING APRIL THE MIST ELIMINATOR PLUGGED CAUSING SYSTEM DOWN TIME.

PROBLEMS WERE ENCOUNTERED WITH THE BOOSTER FAN.

5/81 A 65.4 73.3 75.0 65.4 B .0 .0 .0 .0 .0 SYSTEM 65.4 73.3 75.0 65.4 744

** PROBLEMS/SOLUTIONS/COMMENTS

DURING MAY MODULE A EXPERIENCED BOOSTER FAN PROBLEMS.

6/81 A 72.3 66.3 68.2 52.6 . 0 .0 .0 72.3 SYSTEM 66.3 68.2 52.6 720 571 379 77.9

### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING JUNE MODULE B WAS OUT OF SERVICE FOR MAINTENANCE. MAINTENANCE WAS PERFORMED ON THE SPRAY NOZZLES, MIST ELIMINATOR, TRAY UNDERSPRAY STRAINER, ISOLATION DAMPER, AND THE FLAKE LINING.

MODULE B SPRAY RECYCLE NOZZLES WERE CLEANED AND THE WASH TRAY HEADER WAS CHECKED FOR PLUGGING.

THE RECYCLE TANK TRAY ON MODULE A WAS CLEANED DURING JUNE.

7/81 28.8 32.1 33.3 28.8 A .0 R . 0 . 0 .0 SYSTEM 28.8 32.1 33.3 28.8 744 666 214 82.9

### ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE A WAS REMOVED FROM SERVICE ON JULY 10 WHEN THE THICKENER RAKE DRIVE BROKE. THIS CAUSED THE MODULE TO REMAIN OUT OF SERVICE THE REST OF THE MONTH.

DURING THE MONTH, THE FLAKE LINING WAS BEING REPAIRED ON MODULE B.

NEW MIST ELIMINATORS WERE INSTALLED IN MODULE B DURING JULY.

8/81 A .0 .0 .0 .0 44.2 B 58.1 48.6 49.5 329 79.9 SYSTEM 58.1 48.6 49.5 44.2 744 677

### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING AUGUST, MODULE A WAS OFF LINE AWAITING FAN BLADES AND REPAIRS TO THE ABSORBER TOWER.

MODULE B WAS DOWN FOR PART OF THE MONTH AS REPAIRS CONTINUED TO THE

MINNKOTA POWER: MILTON R. YOUNG 2 (CONT.)

PERIOD	MODULE AV	/AILABILI	TY OPERABILITY	RELIABILÎTY	UTILIZATION	% REMOVAL SO2 PART.				
		+	THICKENER RAKE	DRIVE.						
9/81	A	.0	. 0	.0	. <b>0</b> 85.8					
	B System	100.0 100.0	97.2 97.2	100.0 100.0	85.8 85.8		720	636	618	83.1
	** PROBLE	EMS/SOLUT	IONS/COMMENTS							
			THE UNIT WAS D	OWN TWICE DU	RING THE MON	ITH AS A RESU	JLT OF	BOILER	TUBE I	LEAKS.
			THE A MODULE R	EMAINED DOWN	DURING THE	MONTH FOR RE	PAIRS	•		
0/81	A			53.2	30.8					
	В	35.5	56.9 100.0	60.9	35.3		<b>-</b> //			
							744	461	492	83.0
1/81			98.0	98.9						
	B System	0. 100.0	.0 98.0	98.9	.0 88.9		720	653	640	87.4
	0101211	100.0	, , , ,	,,,,	33.7		, 20	000	0,0	0,,,
2/81	A		21.7							
	B SYSTEM	78.6 100.0	78.6 100.0	79.2 100.0	78.6 100.0		744	744	744	90.1
			IONS/COMMENTS				,		,,,	,,,,
			THE MAJOR PROB	SLEM ENCOUNTE	RED DURING T	THE FOURTH Q	JARTER	WAS FA	ILURE (	)F
			THE FLAKEGLASS	LINERS.						
			SPRAY NOZZLE F	PLUGGING WAS	ALSO ENCOUNT	TERED DURING	THE TI	HREE MOI	NTH PE	RIOD.
1/82	A	17.0	19.1	19.2	17.0					
	В	68.5	77.0	77.7	68.5		=			
			85.5	97.0	85.5		744	662	636	81.7
	** PROBL	EMS/SOLUT	IONS/COMMENTS							
			THE UNIT WAS D							
			DURING THE MON							
			MODULE B WAS T BOOSTER FAN BE			THE REAR B	EARING	TEMPER.	ATURE (	ON THE
			THE ISOLATION	DAMPERS WOUL	D NOT OPERAT	TE DURING TH	E FRIG	ID WEAT	HER.	
2/82		65.9	65.9	65.9	65.9					
	В	31.1	31.1	31.1	31.1					
	SYSTEM	96.9	96.9	96.9	96.9		672	672	651	81.1
3/82		.0	.0		.0					
	B System	55.9 55.9	96.2 96.2	100.0 100.0	55.9 55.9		744	432	61 E	72.]
			IONS/COMMENTS	100.0	33.7		/44	432	413	/2.1
			DURING MARCH 1	THE INTT WEND	[ NOIJN EOD ▲	SCHEDINED A	K/IK/II I A I	OUTACE		
, ,,,,			JUNEAU HARCH	ING ONLI MENI		JUNEBULED A	INUAL	OU! AGE.		
4/82	A B	.0			.0					
	SYSTEM	.0			. 0 . 0		720	0	0	. (
					ی ه		120	U	U	

PERFORMANCE DATA						
PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION	% RE	MOVAL	PER	BOILER	FGD	CAP.
						FACTOR

#### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UNIT WAS OFF-LINE DURING APRIL FOR AN ANNUAL OUTAGE. THE FGD SYSTEM WAS ALSO DOWN FOR THE ENTIRE MONTH.

5/82	A	78. <b>0</b>	88.9	94.9	72.5				
	В	.0	. 0		.0				
	SYSTEM	78.0	88.9	94.9	72.5	744	607	539	76.6

### ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE B WAS DOWN THE MONTH OF MAY BECAUSE OF REPAIRS BEING PERFORMED ON THE FLAKE LINING AND THE SPRAY RECYCLE NOZZLES.

MODULE A WAS DOWN AT THE BEGINNING OF MAY BECAUSE OF THE ANNUAL OUTAGE. LATER IN THE MONTH THE MODULE WAS TAKEN OFF-LINE DUE TO ID FAN PROBLEMS.

6/	82 A	86.2	91.9	93.8	76.4				
	В	.0	.0		.0				
	SYSTEM	86.2	91.9	93.8	76.5	720	599	550	73.5

### ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE B WAS OUT OF SERVICE DURING JUNE BECAUSE WORK WAS BEING PERFORMED ON THE FLAKE LINING AND THE SPRAY RECYCLE NOZZLES.

MODULE A WAS OFF-LINE AT THE BEGINNING OF JUNE DUE TO SCHEDULED MAINTENANCE ON THE TURBINE. THE MODULE WAS ALSO DOWN DURING MID-MONTH WHEN THE BOILER WAS OFF-LINE DUE TO A TUBE LEAK AND TO SET THE LIMIT SWITCHES.

7/82	A-11 A-21 SYSTEM	97.6 .0 97.6	97.6 .0 97.6	100.0	97.6 .0 97.6	744	744	726	80.2
8/82	A-11 A-21 SYSTEM	7.4 96.8 100.0	7.4 92.0 99.4	7.4 92.0 99.4	7.4 92.0 99.4	744	744	740	80.2
9/82	A-11 A-21 SYSTEM	.0 98.9 98.9	.0 98.9 98.9	.0 98.9 98.9	.0 98.9 98.9	720	720	712	81.0

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE PERIOD OF JULY THROUGH SEPTEMBER 1982.

10/82	A-11	50.5	62.6	63.2	50.5				
	A-21	49.5	35.0	35.3	28.3				
	SYSTEM	100.0	97.5	98.5	78.8	744	601	586	75.9

### ** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED BY THE UTILITY. DURING OCTOBER.

11/82	A-11	79.5	77.1	77.8	71.9			
	A-21	.0	.0		.0			
	SYSTEM	79.5	77.1	77.8	71.9	72 <b>0</b>	672	518 62.3

MINNKOTA POWER: MILTON R. YOUNG 2 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

### ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE A-11 WAS DOWN FROM NOVEMBER 16 TO NOVEMBER 22 FOR REPAIR OF LEAKS.

MODULE A-21 WAS OUT OF SERVICE FOR THE ENTIRE MONTH TO ALLOW FOR THE PERFORMANCE OF MAINTENENCE WORK.

12/82 A-11 42.1 48.0 48.9 42.1 A-21 .0 .0 .0 .0 SYSTEM 42.1 48.0 48.9 42.1

744 653 313 65.7

### ** PROBLEMS/SOLUTIONS/COMMENTS

HIGH VIBRATIONS FROM AN ID FAN FORCED THE REMOVAL OF A SET OF FANS ON THE UNIT AND CONSEQUENTLY, AN FGD SYSTEM OUTAGE.

REPAIRS CONTINUED DURING DECEMBER ON THE LEAKS THAT DEVELOPED IN MODULE A-11.

MAINTENANCE WORK CONTINUED DURING THE MONTH ON MODULE A-21.

A DAMAGED COLD REHEAT LINE PRODUCING A LOW VACUUM RESULTED IN A UNIT TRIP ON DECEMBER 10. THE UNIT WAS BROUGHT DOWN ON DECEMBER 13 TO REPAIR THE COLD REHEAT LINE.

1/83 A-11 100.0 97.7 92.3 90.8 A-21 3.0 1.2 1.1 1.1 SYSTEM 100.0 98.9 93.4 91.9

744 692 684 82.6

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING JANUARY.

2/83 A-11 100.0 94.8 86.0 83.7 A-21 .0 .0 .0 .0 SYSTEM 100.0 94.8 86.0 83.7

672 594 562 82.4

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING FEBRUARY.

3/83 A-11 80.6 95.6 94.8 75.7 A-21 .0 .0 .0 .0 SYSTEM . 80.6 95.6 94.8 75.7

744 589 563 77.0

### ** PROBLEMS/SOLUTIONS/COMMENTS

MODULE A-21 HAD BEEN OUT OF SERVICE SINCE OCTOBER AND REMAINED OUT OF SERVICE DURING MARCH FOR REPAIRS TO THE ABSORBER LINING.

THE UNIT WAS TAKEN OUT OF SERVICE ON MARCH 25 FOR A SCHEDULED OUTAGE.

4/83 A-11 33.3 88.1 87.6 29.7 A-21 .0 .0 .0 .0 .0 SYSTEM 33.3 88.1 86.0 29.7

720 243 214 69.5

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE ANNUAL OUTAGE WHICH BEGAN ON MARCH 25 ENDED ON APRIL 20.

WHEN ATTEMPTING TO START A BOOSTER FAN, THE FAN HOUSING FLOODED AND CAUSED

** PROBLEMS/SOLUTIONS/COMMENTS  THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROB DURING JULY.  8/83 A-11 89.4 97.3 97.3 89.4 A-21 .0 0 .0 .0 .0 SYSTEM 89.4 97.3 97.3 89.4 ** PROBLEMS/SOLUTIONS/COMMENTS  WORK CONTINUED DURING AUGUST ON RELINING THE A-21 M MODULE A-11 EXPERIENCED EXPANSION JOINT PROBLEMS DU MODULE A-11 ALSO EXPERIENCED FLYASH SLURRY LINE PROSENTE TO .0 .0 .0 .0 .0 SYSTEM 76.3 89.3 91.2 70.1 ** PROBLEMS/SOLUTIONS/COMMENTS  WORK CONTINUED DURING SEPTEMBER ON RELINING THE A-2 FLYASH SLURRY LINE PROBLEMS CONTINUED DURING SEPTEM MODULE A-11 ALSO EXPERIENCED PROBLEMS WITH THE SPRADURING THE MONTH.  10/63 A-11 16.1 14.4 100.0 13.0 A-21 90.3 83.9 87.3 75.9 SYSTEM 100.0 98.3 100.0 88.9  11/83 A-11 .0 .0 .0 .0 .0 .0 .0 A-21 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 SYSTEM 100.0 SYSTEM 100.0 SYSTEM 100.0 SYSTEM 100.0 SYSTEM SYST	PER 10URS	BOILER HOURS	FGD HOURS	CAP.
A-21 .0 .0 .0 .0 .0 .0 .0 .0 .0 .0 .0 .0 .0				
SYSTEM 98.2 95.4 86.9 84.8  6/83 A-11 99.3 98.4 98.4 94.9  ** PROBLEMS/SOLUTIONS/COMMENTS  THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROB DURING MAY AND JUNE.  7/83 A-11 99.6 98.2 95.3 76.6  ** PROBLEMS/SOLUTIONS/COMMENTS  THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROB DURING MAY AND JUNE.  7/83 A-11 99.6 98.2 95.3 76.6  ** PROBLEMS/SOLUTIONS/COMMENTS  THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROB DURING JULY.  8/83 A-11 89.4 97.3 97.3 89.4  ** PROBLEMS/SOLUTIONS/COMMENTS  MORK CONTINUED DURING AUGUST ON RELINING THE A-21 M  MODULE A-11 EXPERIENCED EXPANSION JOINT PROBLEMS DU  HODULE A-11 ALSO EXPERIENCED FLYASH SLURRY LINE PRO  9/83 A-11 76.3 89.3 91.2 70.1  A-21 .0 .0 .0 .0 .0  SYSTEM 76.3 89.3 91.2 70.1  ** PROBLEMS/SOLUTIONS/COMMENTS  WORK CONTINUED DURING SEPTEMBER ON RELINING THE A-2  FLYASH SLURRY LINE PROBLEMS CONTINUED DURING SEPTEM  MODULE A-11 ALSO EXPERIENCED PROBLEMS WITH THE SPRA  DURING THE MONTH.  10/83 A-11 16.1 14.4 100.0 13.0  A-21 90.3 83.9 87.3 75.9  SYSTEM 100.0 98.3 100.0 88.9  11/83 A-11 0. 0 0.0 .0  ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURING  ** PROBLEMS/SOLUTIONS/COMMENTS				
6/83 A-11 99.3 98.4 98.4 94.9 A-21 .0 .0 .0 .0 .0 SYSTEM 99.3 98.4 98.4 94.9  ** PROBLEMS/SOLUTIONS/COMMENTS  THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROB DURING MAY AND JUNE.  7/83 A-11 99.6 98.2 95.3 76.6 A-21 .0 .0 .0 .0 .0 SYSTEM 99.6 98.2 95.3 76.6  ** PROBLEMS/SOLUTIONS/COMMENTS  THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROB DURING JULY.  8/83 A-11 89.4 97.3 97.3 89.4 A-21 .0 .0 .0 .0 .0 .0 SYSTEM 89.4 97.3 97.3 89.4  ** PROBLEMS/SOLUTIONS/COMMENTS  #* PROBLEMS/SOLUTIONS/COMMENTS  HORK CONTINUED DURING AUGUST ON RELINING THE A-21 M MODULE A-11 ALSO EXPERIENCED EXPANSION JOINT PROBLEMS DU HODULE A-11 ALSO EXPERIENCED FLYASH SLURRY LINE PROBLEMS/SOLUTIONS/COMMENTS  #* PROBLEMS/SOLUTIONS/COMMENTS  MORK CONTINUED DURING SEPTEMBER ON RELINING THE A-2 FLYASH SLURRY LINE PROBLEMS/SOLUTIONS/COMMENTS  #* PROBLEMS/SOLUTIONS/COMMENTS  MORK CONTINUED DURING SEPTEMBER ON RELINING THE A-2 FLYASH SLURRY LINE PROBLEMS CONTINUED DURING SEPTEM MODULE A-11 ALSO EXPERIENCED PROBLEMS WITH THE SPRA DURING THE MONTH.  10/83 A-11 16.1 14.4 100.0 13.0 A-21 90.3 83.9 87.3 75.9 SYSTEM 100.0 98.3 100.0 88.9  11/83 A-11 00 .0 .0 .0 .0 .0 .0 SYSTEM 100.0 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 SYSTEM 100.0 SYSTEM 100.0 100.0 100.0 SYSTEM 100.0	744		(71	07.0
SYSTEM   99.3   98.4   98.4   94.9	744	661	631	83.8
SYSTEM   99.3   98.4   98.4   94.9				
** PROBLEMS/SOLUTIONS/COMMENTS  THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROB DURING MAY AND JUNE.  7/83	720	695	683	83.5
## PROBLEMS/SOLUTIONS/COMMENTS  *# PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURINS  *## PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURINS  NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURINS				
A-21 .0 .0 .7 .0 .7 .0 .9 .9 .5	BLEMS	WERE E	ENCOUNT	ERED
SYSTEM 99.6 98.2 95.3 76.6  *** PROBLEMS/SOLUTIONS/COMMENTS  THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROB DURING JULY.  8/83 A-11 89.4 97.3 97.3 89.4 A-21 .0 .0 .0 .0 .0 SYSTEM 89.4 97.3 97.3 89.4  *** PROBLEMS/SOLUTIONS/COMMENTS  WORK CONTINUED DURING AUGUST ON RELINING THE A-21 M MODULE A-11 EXPERIENCED EXPANSION JOINT PROBLEMS DU MODULE A-11 ALSO EXPERIENCED FLYASH SLURRY LINE PROBLEMS/SOLUTIONS/COMMENTS  *** PROBLEMS/SOLUTIONS/COMMENTS  WORK CONTINUED DURING SEPTEMBER ON RELINING THE A-2 FLYASH SLURRY LINE PROBLEMS/SOLUTIONS/COMMENTS  WORK CONTINUED DURING SEPTEMBER ON RELINING THE A-2 FLYASH SLURRY LINE PROBLEMS CONTINUED DURING SEPTEM MODULE A-11 ALSO EXPERIENCED PROBLEMS WITH THE SPRADURING THE MONTH.  10/83 A-11 16.1 14.4 100.0 13.0 A-21 90.3 83.9 87.3 75.9 SYSTEM 100.0 98.3 100.0 88.9  11/83 A-11 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0				
## PROBLEMS/SOLUTIONS/COMMENTS  THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROB DURING JULY.  8/83	744	. 500	570	01 5
THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROB DURING JULY.  8/83 A-11 89.4 97.3 97.3 89.4 A-21 .0 .0 .0 .0 .0 SYSTEM 89.4 97.3 97.3 89.4  *** PROBLEMS/SOLUTIONS/COMMENTS  WORK CONTINUED DURING AUGUST ON RELINING THE A-21 M MODULE A-11 EXPERIENCED EXPANSION JOINT PROBLEMS DU MODULE A-11 ALSO EXPERIENCED FLYASH SLURRY LINE PRO  9/83 A-11 76.3 89.3 91.2 70.1 A-21 .0 .0 .0 .0 .0 SYSTEM 76.3 89.3 91.2 70.1  *** PROBLEMS/SOLUTIONS/COMMENTS  WORK CONTINUED DURING SEPTEMBER ON RELINING THE A-2 FLYASH SLURRY LINE PROBLEMS CONTINUED DURING SEPTEM MODULE A-11 ALSO EXPERIENCED PROBLEMS WITH THE SPRA DURING THE MONTH.  10/83 A-11 16.1 14.4 100.0 13.0 A-21 90.3 83.9 87.3 75.9 SYSTEM 100.0 98.3 100.0 88.9  11/83 A-11 .0 .0 .0 .0 A-21 100.0 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 100.0 *** PROBLEMS/SOLUTIONS/COMMENTS	/44	, 30U	5/0	01.5
A-21 .0 .0 .0 .0 .0  SYSTEM 89.4 97.3 97.3 89.4  ** PROBLEMS/SOLUTIONS/COMMENTS  WORK CONTINUED DURING AUGUST ON RELINING THE A-21 M  MODULE A-11 EXPERIENCED EXPANSION JOINT PROBLEMS DU  MODULE A-11 ALSO EXPERIENCED FLYASH SLURRY LINE PRO  9/83 A-11 76.3 89.3 91.2 70.1  A-21 .0 .0 .0 .0 .0  SYSTEM 76.3 89.3 91.2 70.1  ** PROBLEMS/SOLUTIONS/COMMENTS  WORK CONTINUED DURING SEPTEMBER ON RELINING THE A-2  FLYASH SLURRY LINE PROBLEMS CONTINUED DURING SEPTEM  MODULE A-11 ALSO EXPERIENCED PROBLEMS WITH THE SPRA  DURING THE MONTH.  10/83 A-11 16.1 14.4 100.0 13.0  A-21 90.3 83.9 87.3 75.9  SYSTEM 100.0 98.3 100.0 88.9  11/83 A-11 .0 .0 .0 .0  A-21 100.0 100.0 100.0 100.0  SYSTEM 100.0 100.0 100.0 100.0  ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURIN	BLEMS	WERE E	ENCOUNT	ERED
A-21 .0 .0 .0 .0 .0  SYSTEM 89.4 97.3 97.3 89.4  ** PROBLEMS/SOLUTIONS/COMMENTS  WORK CONTINUED DURING AUGUST ON RELINING THE A-21 M  MODULE A-11 EXPERIENCED EXPANSION JOINT PROBLEMS DU  MODULE A-11 ALSO EXPERIENCED FLYASH SLURRY LINE PRO  9/83 A-11 76.3 89.3 91.2 70.1  A-21 .0 .0 .0 .0 .0  SYSTEM 76.3 89.3 91.2 70.1  ** PROBLEMS/SOLUTIONS/COMMENTS  WORK CONTINUED DURING SEPTEMBER ON RELINING THE A-2  FLYASH SLURRY LINE PROBLEMS CONTINUED DURING SEPTEM  MODULE A-11 ALSO EXPERIENCED PROBLEMS WITH THE SPRA  DURING THE MONTH.  10/83 A-11 16.1 14.4 100.0 13.0  A-21 90.3 83.9 87.3 75.9  SYSTEM 100.0 98.3 100.0 88.9  11/83 A-11 .0 .0 .0 .0  A-21 100.0 100.0 100.0 100.0  SYSTEM 100.0 100.0 100.0 100.0  ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURIN				
** PROBLEMS/SOLUTIONS/COMMENTS  WORK CONTINUED DURING AUGUST ON RELINING THE A-21 M  MODULE A-11 EXPERIENCED EXPANSION JOINT PROBLEMS DU  MODULE A-11 ALSO EXPERIENCED FLYASH SLURRY LINE PRO  9/83 A-11 76.3 89.3 91.2 70.1  A-21 .0 .0 .0 .0 .0  SYSTEM 76.3 89.3 91.2 70.1  ** PROBLEMS/SOLUTIONS/COMMENTS  WORK CONTINUED DURING SEPTEMBER ON RELINING THE A-2  FLYASH SLURRY LINE PROBLEMS CONTINUED DURING SEPTEM  MODULE A-11 ALSO EXPERIENCED PROBLEMS WITH THE SPRA DURING THE MONTH.  10/83 A-11 16.1 14.4 100.0 13.0  A-21 90.3 83.9 87.3 75.9  SYSTEM 100.0 98.3 100.0 88.9  11/83 A-11 .0 .0 .0 .0  A-21 100.0 100.0 100.0 88.9  11/83 A-11 .0 .0 .0 .0  ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURIN				
## WORK CONTINUED DURING AUGUST ON RELINING THE A-21 M  ## MODULE A-11 EXPERIENCED EXPANSION JOINT PROBLEMS DU  ## PROBLEMS/SOLUTIONS/COMMENTS  ## PROBLEMS ## 16.1	744	684	665	89.5
MODULE A-11 EXPERIENCED EXPANSION JOINT PROBLEMS DU  MODULE A-11 ALSO EXPERIENCED FLYASH SLURRY LINE PRO  9/83 A-11 76.3 89.3 91.2 70.1 A-21 .0 .0 .0 .0 .0 SYSTEM 76.3 89.3 91.2 70.1  *** PROBLEMS/SOLUTIONS/COMMENTS  WORK CONTINUED DURING SEPTEMBER ON RELINING THE A-2 FLYASH SLURRY LINE PROBLEMS CONTINUED DURING SEPTEM  MODULE A-11 ALSO EXPERIENCED PROBLEMS WITH THE SPRA DURING THE MONTH.  10/83 A-11 16.1 14.4 100.0 13.0 A-21 90.3 83.9 87.3 75.9 SYSTEM 100.0 98.3 100.0 88.9  11/83 A-11 .0 .0 .0 .0 A-21 100.0 100.0 100.0 88.9  11/83 A-11 .0 .0 .0 SYSTEM 100.0 100.0 100.0 100.0 *** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURIN				
## PROBLEMS/SOLUTIONS/COMMENTS  MODULE A-11 ALSO EXPERIENCED FLYASH SLURRY LINE PROPRIET OF THE MODULE A-11 ALSO EXPERIENCED PROBLEMS WITH THE SPRA DURING THE MONTH.  MORK CONTINUED DURING SEPTEMBER ON RELINING THE A-2 FLYASH SLURRY LINE PROBLEMS CONTINUED DURING SEPTEM MODULE A-11 ALSO EXPERIENCED PROBLEMS WITH THE SPRA DURING THE MONTH.  10/83 A-11 16.1 14.4 100.0 13.0 A-21 90.3 83.9 87.3 75.9 SYSTEM 100.0 98.3 100.0 88.9  11/83 A-11 .0 .0 .0 .0 .0 A-21 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 100.0 100.0 *** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURING	100UL	E ABSOR	RBER TO	WER.
9/83 A-11 76.3 89.3 91.2 70.1 A-21 .0 .0 .0 .0 .0 SYSTEM 76.3 89.3 91.2 70.1  ** PROBLEMS/SOLUTIONS/COMMENTS  WORK CONTINUED DURING SEPTEMBER ON RELINING THE A-2 FLYASH SLURRY LINE PROBLEMS CONTINUED DURING SEPTEM  MODULE A-11 ALSO EXPERIENCED PROBLEMS WITH THE SPRA DURING THE MONTH.  10/83 A-11 16.1 14.4 100.0 13.0 A-21 90.3 83.9 87.3 75.9 SYSTEM 100.0 98.3 100.0 88.9  11/83 A-11 .0 .0 .0 .0 A-21 100.0 100.0 100.0 88.9  11/83 A-11 .0 .0 .0 SYSTEM 100.0 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 100.0 SYSTEM 100.0 FGD-RELATED OUTAGES WERE ENCOUNTERED DURING	JRING	AUGUS1	г.	
## PROBLEMS/SOLUTIONS/COMMENTS  WORK CONTINUED DURING SEPTEMBER ON RELINING THE A-2  FLYASH SLURRY LINE PROBLEMS CONTINUED DURING SEPTEM  MODULE A-11 ALSO EXPERIENCED PROBLEMS WITH THE SPRA  DURING THE MONTH.  10/83 A-11 16.1 14.4 100.0 13.0  A-21 90.3 83.9 87.3 75.9  SYSTEM 100.0 98.3 100.0 88.9  11/83 A-11 .0 .0 .0 .0  A-21 100.0 100.0 100.0 100.0  SYSTEM 100.0 100.0 100.0 100.0  ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURING	OB LEM	15 DURIN	NG THE	монтн.
## PROBLEMS/SOLUTIONS/COMMENTS    WORK CONTINUED DURING SEPTEMBER ON RELINING THE A-2				
** PROBLEMS/SOLUTIONS/COMMENTS  WORK CONTINUED DURING SEPTEMBER ON RELINING THE A-2  FLYASH SLURRY LINE PROBLEMS CONTINUED DURING SEPTEM  MODULE A-11 ALSO EXPERIENCED PROBLEMS WITH THE SPRA  DURING THE MONTH.  10/83 A-11 16.1 14.4 100.0 13.0  A-21 90.3 83.9 87.3 75.9  SYSTEM 100.0 98.3 100.0 88.9  11/83 A-11 .0 .0 .0 .0  A-21 100.0 100.0 100.0 100.0  SYSTEM 100.0 100.0 100.0 100.0  ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURIN	720	566	505	00.0
WORK CONTINUED DURING SEPTEMBER ON RELINING THE A-2  FLYASH SLURRY LINE PROBLEMS CONTINUED DURING SEPTEM  MODULE A-11 ALSO EXPERIENCED PROBLEMS WITH THE SPRA DURING THE MONTH.  10/83 A-11 16.1 14.4 100.0 13.0 A-21 90.3 83.9 87.3 75.9 SYSTEM 100.0 98.3 100.0 88.9  11/83 A-11 .0 .0 .0 A-21 100.0 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 100.0 ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURIN	720	, 566	505	00.2
FLYASH SLURRY LINE PROBLEMS CONTINUED DURING SEPTEM  MODULE A-11 ALSO EXPERIENCED PROBLEMS WITH THE SPRA DURING THE MONTH.  10/83 A-11 16.1 14.4 100.0 13.0 A-21 90.3 83.9 87.3 75.9 SYSTEM 100.0 98.3 100.0 88.9  11/83 A-11 .0 .0 .0 .0 A-21 100.0 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 100.0 *** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURIN				
MODULE A-11 ALSO EXPERIENCED PROBLEMS WITH THE SPRADURING THE MONTH.  10/83 A-11 16.1 14.4 100.0 13.0 A-21 90.3 83.9 87.3 75.9 SYSTEM 100.0 98.3 100.0 88.9  11/83 A-11 .0 .0 .0 .0 .0 A-21 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 100.0 100.0 100.0 100.0 NYSTEM 100.0 100.0 100.0 100.0 100.0 NYSTEM 100.0 TOO TOO TOO TOO TOO TOO TOO TOO TOO TO	21 MO	DDULE A	BSORBER	TOWER.
DURING THE MONTH.  10/83	MBER	AT THE	A-11 M	ODULE.
A-21 90.3 83.9 87.3 75.9 SYSTEM 100.0 98.3 100.0 88.9  11/83 A-11 .0 .0 .0 .0 A-21 100.0 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 100.0 ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURIN	AY RE	ECYCLE I	PUMP ST	RAINERS
SYSTEM 100.0 98.3 100.0 88.9  11/83 A-11 .0 .0 .0 .0 A-21 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURIN				
11/83 A-11 .0 .0 .0 .0 A-21 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 100.0 *** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURIN	744			00.0
A-21 100.0 100.0 100.0 100.0 SYSTEM 100.0 100.0 100.0 100.0 ** PROBLEMS/SOLUTIONS/COMMENTS NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURIN	744	4 673	662	89.8
SYSTEM 100.0 100.0 100.0 100.0  ** PROBLEMS/SOLUTIONS/COMMENTS  NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURIN				
** PROBLEMS/SOLUTIONS/COMMENTS NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURIN	720	720	720	87.4
NO MAJOR FGD-RELATED OUTAGES WERE ENCOUNTERED DURIN	, 20	,,,,	, 20	07.4
		_		
1983.	NG OC	CTOBER	VON DNA	EMBER
12/83 A-11 .0 .0 .0				

MINNKOTA POWER: MILTON R. YOUNG 2 (CONT.)

8/84 SYSTEM

9/84 SYSTEM

ERIOD	MODULE		OPERABILITY		UTILIZATION	<b>S</b> 02	PART.	HOURS	HOURS	HOURS	FACTOR
	A-21 SYSTEM	70.1 70.1	78.1 78.1	54.3 54.3	54.3 54.3			744	518	404	75.6
	** PROE	LEMS/SOLUTIO	NS/COMMENTS								
		t	10DULE A-11 W	AS BEING REL	INED DURING D	ECEMBE	R.				
			MAINTENANCE W								CYCLE
			THREE UNIT OU DROGEN LEAK R		ED DURING DEC	CEMBER	DUE TO	O BOIL	ER TUBE	LEAK	AND HY-
1/84	A-11	.0	.0	.0	.0						
	A-21	.0 84.5	.0 84.5 84.5	100.0	84.5						
	SYSTEM	84.5	84.5	100.0	84.5			744	744	629	87.8
	** PROB	LEMS/SOLUTIO	NS/COMMENTS								
		ľ	10DULE A-11 W	AS NOT AVAIL	ABLE FOR SERV	/ICE DU	E TO I	MODULE	RELINI	NG.	
			THE UTILITY R 10DULE A21 SP			NAS SI	ים דטו	оми то	MAKE R	EPAIRS	ON
2/84	A-11	3.4	.0 100.0		.0						
	A-21	100.0	100.0	100.0	100.0						
			100.0					696	696	696	78.4
3/84	A-11	100.0	.0 100.0 100.0		.0						
	A-21	100.0	100.0	100.0	100.0						
								744		744	76.8
4/84	A-11	100.0	.0 99.1		.0						
	A-21	100.0	99.1	99.8	88.3						
	SYSTEM	100.0	99.1	99.8	88.3			720	641	<b>6</b> 36	74.7
	** PROB	BLEMS/SOLUTION	ONS/COMMENTS								
			THE UTILITY R PERIOD OF FEB				ED PR	OBLEMS	AROSE	DURING	THE
5/84		100.0			.0						
	A-21	_			.0				_	_	_
		100.0			.0			744	0	0	.0
	** PROE	BLEMS/SOLUTI	ONS/COMMENTS								
		,	THE UNIT WAS	SHUT DOWN TH	ROUGHOUT MAY	FOR IT	S ANN	UAL OU	TAGE.		
6/84	A-11	. 0	.0		.0						
	A-21		89.8	105.5	45.6						
	SYSTEM		89.8	100.0	45.6			720	366	328	79.4
	** PROS	BLEMS/SOLUTI	ONS/COMMENTS								
			THE UTILITY R	EPORTED THAT	NO MAJOR EGI	D-RELAT	ED PR	OBLEMS	AROSE	DURTNG	JUNE.

744

720

 		 DEDEODMA	UCE DATA						
	AVAILABILITY	_							
				502	PART.	HOURS	HOURS	HOURS	FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE THIRD QUARTER OF 1984.

### SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

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MONONGAHELA POWER COMPANY NAME PLEASANTS PLANT NAME UNIT NUMBER WILLOW ISLAND CITY WEST VIRGINIA STATE D 21. ( .050 LB/MMBTU) 516. ( 1.200 LB/MMBTU) 301. ( .700 LB/MMBTU) 1160 REGULATORY CLASSIFICATION PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW
GROSS UNIT GENERATING CAPACITY - MW
NET UNIT GENERATING CAPACITY W/FGD - MW
NET UNIT GENERATING CAPACITY WO/FGD - MW 626 580 595 626 EQUIVALENT SCRUBBED CAPACITY - MW ** UNIT DATA - BOILER AND STACK BOILER SUPPLIER FOSTER WHEELER BOILER TYPE PULVERIZED COAL BOILER SERVICE LOAD BASE DESIGN BOILER FLUE GAS FLOW - CU.M/S 1132.56 (2400000 ACFM)
BOILER FLUE GAS TEMPERATURE - C 132.2 (270 F)
STACK HEIGHT - M 305. (1000 FT)
STACK SHELL CONCRETE
STACK TOP DIAMETER - M 6.1 (20.0 FT) ** FUEL DATA FUEL TYPE COAL BITUMINOUS FUEL GRADE 29075. ( 12500 BTU/LB) AVERAGE HEAT CONTENT - J/G RANGE HEAT CONTENT - BTU/LB 11000-13300 ****** AVERAGE ASH CONTENT - % RANGE ASH CONTENT - % 14.7-16.0 AVERAGE MOISTURE CONTENT - %
RANGE MOISTURE CONTENT - %
AVERAGE SULFUR CONTENT - % 4.50 3.0-5.0 3.00 2.5-3.5 RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % .05 RANGE CHLORIDE CONTENT - % *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER 0 TYPE NONE ** FABRIC FILTER NUMBER n TYPE NONE ** ESP NUMBER 2 NUMBER OF SPARES 0 COLD SIDE SUPPLIER AIR CORRECTION DIVISION, UOP INLET FLUE GAS CAPACITY - CU.M/S
INLET FLUE GAS TEMPERATURE - C
PARTICLE REMOVAL EFFICENCY - % 566.3 (1200000 ACFM) 132.2 ( 270 F) 99.5 ** PARTICLE SCRUBBER NUMBER GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL N/A LINER GENERIC MATERIAL N/A LINER SPECIFIC MATERIAL

N/A

### *** FGD SYSTEM

```
** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                              THROWAWAY PRODUCT
   SO2 REMOVAL MODE
                                              WET SCRUBBING
                                              LIME
   PROCESS TYPE
   PROCESS ADDITIVES
                                              NONE
   SYSTEM SUPPLIER
                                              BABCOCK & WILCOX
   A-F FTRM
                                              UNITED ENGINEERS & CONSTRUCTORS
   DEVELOPMENT LEVEL
                                              FULL SCALE
   NEW/RETROFIT
                                              NEW
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.55
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - X
                                                 90.00
    ENERGY CONSUMPTION - %
                                                 2.4
   CURRENT STATUS
                                               1
    COMMERCIAL START-UP
                                              12/80
   INITIAL START-UP
                                              12/78
    CONTRACT AWARDED
                                               9/75
** DESIGN AND OPERATING PARAMETERS
   DESIGN COAL SULFER CONTENT - %
                                                4.50
   DESIGN COAL HEAT CONTENT - J/G
                                             28842.4
                                                             ( 12400 RTIL/LB)
   DESIGN COAL ASH CONTENT - %
                                               16.00
   DESIGN MOISTURE CONTENT - %
                                                  5.00
   DESIGN CHLORIDE CONTENT - %
                                                   .05
    SPACE REQUIREMENTS - SQ M
                                              20252.2
                                                             ( 218000 SQ FT)
    OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                               208.0
** QUENCHER/PRESATURATOR
   NUMBER
    TYPE
                                              VENTURI
   SUPPLIER
                                              BABCOCK & WILCOX
    INLET GAS FLOW - CU. M/S
                                                283.14 ( 600000 ACFM)
    INLET GAS TEMPERATURE - C
                                                148.9
                                                            ( 300 F)
    PRESSURE DROP - KPA
                                                           ( 4.0 IN-H20)
                                                 1.0
    LIQUID RECIRCULATION RATE - LITERS/S
                                               504.
                                                            ( 8000 GPM)
    L/G RATIO - L/CU. M
                                                            ( 13.3 GAL/1000 ACFM)
                                                  1.8
    CONSTRUCTION MATERIAL GENERIC TYPE
                                             CARBON STEEL
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                             AISI 1110
** ABSORBER
                                               4
   NUMBER
    NUMBER OF SPARES
                                               1
                                              TRAY TOWER
    GENERIC TYPE
    SPECIFIC TYPE
                                              SIEVE TRAY
    TRADE NAME/COMMON TYPE
                                              N/A
    SUPPLIER
                                              BABCOCK & WILCOX
    SHELL GENERIC MATERIAL
                                              CARBON STEEL
    SHELL SPECIFIC MATERIAL
                                              AISI 1110
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                              N/A
    LINER GENERIC MATERIAL
                                             ORGANIC
    LINER SPECIFIC MATERIAL
                                             SYNTHETIC RUBBER
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                             CHLOROBUTYL
    GAS CONTACTING DEVICE TYPE
                                              PERFORATED TRAYS
   NUMBER OF CONTACTING ZONES
                                              1
    LIQUID RECIRCULATION RATE - LITER/S
                                              1008.
                                                            (16000 GPM)
                                                 4.0
                                                            ( 30.2 GAL/1000 ACF)
    L/G RATIO - L/CU.M
                                                  1.2
                                                             ( 5.0 IN-H20)
    GAS-SIDE PRESSURE DROP - KPA
    SUPERFICAL GAS VELOCITY - M/SEC
                                                  3.0
                                                            ( 10.0 FT/S)
                                               250.11
                                                            ( 530000 ACFM)
    INLET GAS FLOW - CU. M/S
                                                 51.7
                                                            ( 125 F)
    INLET GAS TEMPERATURE - C
   SO2 REMOVAL EFFICIENCY %
                                                 90.0
** MIST ELIMINATOR
   PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                            PRIMARY COLLECTOR
   NUMBER PER SYSTEM
                                               4
   NUMBER OF SPARES PER SYSTEM
                                               1
   NUMBER PER MODULE
                                               1
                                              IMPINGEMENT
   GENERIC TYPE
                                              RAFFIE
   SPECIFIC TYPE
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MONONGAHELA POWER: PLEASANTS 1 (CONT.)

	TRADE NAME/COMMON TYPE  MANUFACTURER  CONFIGURATION  NUMBER OF STAGES  NUMBER OF PASSES PER STAGE  DISTANCE BETWEEN STAGES - CM  SUPERFICAL GAS VELOCITY - M/S  CONSTRUCTION MATERIAL GENERIC TYPE  CONSTRUCTION MATERIAL SPECIFIC TYPE  WASH WATER SOURCE  WASH FREQUENCY  WASH RATE - L/S	3.0 ORGANIC FIBER-REINFOR THICKENER OVE	(84.0 IN) (10.0 FT/S)  RCED POLYESTER ERFLOW/MAKEUP GONCE EVERY 2 HOURS (240 GAL/MIN)
**	REHEATER	_	
	NUMBER NUMBER OF SPARES	1	
	GENERIC TYPE	BYPASS	
	SPECIFIC TYPE	COLD SIDE	
	TRADE NAME/COMMON TYPE	N/A	-v
	LOCATION PERCENT GAS BYPASSED - AVG	AHEAD OF STAC	<i>.</i> ∧
	TEMPERATURE INCREASE - C	13.9	( 25 F)
	INLET FLUE GAS TEMPERATURE - C	51.7	( 125 F)
	OUTLET FLUE GAS TEMPERATURE - C CONSTRUCTION MATERIAL GENERIC TYPE	65.6 NR	( 150 F)
	CONSTRUCTION MATERIAL SPECIFIC TYPE	NR	
××	FANS		
	NUMBER	4	
	NUMBER OF SPARES DESIGN	0 CENTRIFUGAL	
	SUPPLIER	AMERICAN STAN	NDARD
	FUNCTION	BOOSTER	
	APPLICATION	FORCED DRAFT	
	SERVICE FLUE GAS FLOW RATE - CU.M/S	DRY 267.10	( 566000 ACFM)
	FLUE GAS TEMPERATURE - C	132.2	( 270 F)
	PRESSURE DROP - KPA		(26.0 IN-H2O)
	CONSTRUCTION MATERIAL GENERIC TYPE	CARBON STEEL	
××	FANS	_	
	NUMBER NUMBER OF SPARES	2 0	
	DESIGN	NR NR	
	SUPPLIER	AMERICAN STAR	NDARD
	FUNCTION	UNIT	
	APPLICATION SERVICE	FORCED DRAFT DRY	
	FLUE GAS FLOW RATE - CU.M/S	493.14	(1045000 ACFM)
	FLUE GAS TEMPERATURE - C	132.2	( 270 F)
	PRESSURE DROP - KPA CONSTRUCTION MATERIAL GENERIC TYPE	7.6 CARBON STEEL	(25.0 IN-H20)
**	_		
	DAMPERS NUMBER	4	
	FUNCTION	SHUT-OFF	
	GENERIC TYPE	LOUVER	
	SPECIFIC TYPE MANUFACTURER		DSED BLADE MULTILOUVER
	SERVICE CONDITIONS	FORNEY ENGIN	EERING
	CONSTRUCTION MATERIAL GENERIC TYPE	CARBON STEEL	
	CONSTRUCTION MATERIAL SPECIFIC TYPE		H LOW ALLOY [HSLA]
	LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	NONE N/A	
¥×			
	DAMPERS NUMBER	4	
	FUNCTION	SHUT-OFF	
	GENERIC TYPE	LOUVER	
	SPECIFIC TYPE MANUFACTURER	PARALLEL/OPP FORNEY ENGIN	OSED BLADE MULTILOUVER
		EARTHET ENGIN	LLKING

### MONONGAHELA POWER: PLEASANTS 1 (CONT.)

SERVICE CONDITIONS
CONSTRUCTION MATERIAL GENERIC TYPE
CONSTRUCTION MATERIAL SPECIFIC TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

125 STAINLESS STEEL AUSTENITIC NONE N/A

#### ** DUCTWORK

LOCATION
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

INLET
CARBON STEEL
AISI 1110
NONE
N/A

#### ** DUCTWORK

LOCATION
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

OUTLET
CARBON STEEL
AISI 1110
ORGANIC; INORGANIC
ASPHALT-URETHANE; BOROSILICATE GLASS

#### ** DUCTWORK

LOCATION
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

OUTLET AFTER BYPASS JUNCTION CARBON STEEL AISI 1110

INORGANIC

### ** DUCTWORK

LOCATION
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

BYPASS CARBON STEEL AISI 1110 NONE N/A

### ** REAGENT PREPARATION EQUIPMENT

FUNCTION
DEVICE
DEVICE TYPE
MANUFACTURER
NUMBER
NUMBER OF SPARES
PRODUCT QUALITY - % SOLIDS

SLAKER
DETENTION
N/A
DOPR-OLIVER
3
1

### ** TANKS SERVICE

RECIRCULATION
ME WASH
SLURRY TRANSFER
SLURRY FEED
THICKENER OVERFLOW
SLUDGE STABILIZATION

NUMBER

### ** PUMPS

SERVICE
-----QUENCHER RECIRCULATION
ABSORBER RECIRCULATION
THICKENER UNDERFLOW
LIME SLURRY TRANSFER
LIME SLURRY FEED
SLUDGE TRANSFER
RETURN WATER

### NUMBER

### ** SOLIDS CONCENTRATING/DEWATERING

DEVICE NUMBER NUMBER OF SPARES CONFIGURATION DIMENSIONS FT CAPACITY THICKENER 2

0 CIRCULAR 175.0 DIA X 10.0 2190000

MONONGAHELA POWER: PLEASANTS 1 (CONT.)

CARBON STEEL SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE AISI 1110 LINER GENERIC MATERIAL TYPE ORGANIC COAL TAR EPOXY ABSORBER BLEED LINER SPECIFIC MATERIAL TYPE FEED STREAM SOURCE FEED STREAM CHARACTERISTICS 6% SOLIDS 30% SOLIDS [27-32%], PH 8.0 OUTLET STREAM CHARACTERISTICS OUTLET STREAM DISPOSITION TO SLUDGE TREATMENT OVERFLOW STREAM DISPOSITION RECIRCULATION TANK

*** SALEABLE BYPRODUCTS

NATURE

NONE

*** SLUDGE

** TREATMENT

METHOD

DEVICE

PROPRIETARY PROCESS

PROPRIETARY PROCESS INLET QUALITY - %

** DISPOSAL

NATURE

TYPE

LCCATION

SITE TRANSPORTATION METHOD

SITE TREATMENT

SITE DIMENSIONS

SITE SERVICE LIFE - YRS

** PROCESS CONTROL AND INSTRUMENTATION

PROCESS STREAM
CHEMICAL PARAMETERS
PHYSICAL VARIABLES
CONTROL LEVELS
MONITOR TYPE
MONITOR LOCATION

** WATER BALANCE
WATER LOOP TYPE
RECEIVING WATER STREAM
SOURCE OF MAKEUP WATER

** CHEMICALS AND CONSUMPTION FUNCTION NAME PRINCIPAL CONSTITUENT

SOURCE/SUPPLIER CONSUMPTION UTILIZATION - % POINT OF ADDITION

** FGD SPARE CAPACITY INDICES

ABSOREER %
FAN - %
SLAKER %
THICKENER - %

** FGD SPARE COMPONENT INDICES

ABSORBER FAN SLAKER THICKENER FIXATION MIX TANK DRAVO [CALCILOX] 30.0

FINAL
POND
OFF-SITE [1.5 MILES]
PIPELINE
NONE
200 ACRES X 200 FT
31

OUTLET FROM ABSORBER
PH, SO2
DENSITY, FLOW
PH 5.9-6.0, 6% SOLIDS IN SLURRY
UNILOC [PH], LEAR SIEGLER [SO2], TEXAS NUCLEAR [
ABSORBER DOWNCOMER FOR PH

CLOSED
OHIO RIVER
RIVER WATER AND COOLING TOWER BLOWDOWN

ABSORBENT
THIOSORBIC LIME
>90% CAO, 4-7% MGO
DRAVO
11.1 TPH
94.0
SLAKER

33.3

.0 1.0 .0

1.0

.0 1.0 .0

720

6/80 SYSTEM

ERIOD	MODULE	AVAILA	ABILI	TY OPERABILITY RELIABILITY UTILIZATION				BOILER HOURS		
3/79	SYSTEM						744			
4/79	SYSTEM						720			
	** PROS	BLEMS/S	SOLUT	IONS/COMMENTS						
				THE UNIT STARTED ON MARCH 7, 1979. NOT THE RECENT OPERATING STATUS.	HOUR	S ARE	YET AVA	AILABLE	BECAUS	SE OF
				THE A-MODULE HAS BEEN REMOVED FROM SER ABSORBER DOWNCOMER SECTION.	RVICE	DUE TO	A WELD	) FAILU	RE ON 1	THE
5/79	SYSTEM						744			
6/79	SYSTEM						720			
	** PRO	BLEMS/	SOLUT	IONS/COMMENTS						
				THE UTILITY REPORTED THAT THE UNIT WAS DUE TO SEVERE STACK LINER FAILURE. THE SERVICE UNTIL THE MIDDLE OF AUGUST.				_		
7/79	SYSTEM		. 0	.0			744	0	0	.0
8/79	SYSTEM		.0	.0			744	0	0	.0
9/79	SYSTEM		.0	.0			720	0	0	.0
	** PRO	BLEMS/S	SOLUT	IONS/COMMENTS						
				THE UNIT RESTARTED IN LATE SEPTEMBER A	AFTER	COMPLE	TION OF	F THE S	TACK	
10/79	SYSTEM						744			
11/79	SYSTEM						720			
L2/7 <b>9</b>	SYSTEM						744			
	** PROS	BLEMS/	SOLUT	IONS/COMMENTS						
				NO INFORMATION WAS AVAILABLE FOR THIS	REPOR	T PERI	OD.			
1/80	SYSTEM						744			
2/80	SYSTEM						690			
3/80	SYSTEM						744			
	** PRO	BLEMS/	SOLUT	IONS/COMMENTS						
				NO INFORMATION WAS AVAILABLE ON THE OFFIRST QUARTER OF 1980.	PERATI	ONS AT	PLEAS	ANTS 1	FOR TH	E
4/80	SYSTEM						720			
5/80	SYSTEM						744			

MONONGAHELA POWER: PLEASANTS I (CONT.)

PERFORMANCE DATA					
PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION	% REMUVAL	PER	DOILER	FGU	CAP.
	SO2 PART.	HOURS	HOURS	HOURS	FACTOR

### ** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE SECOND QUARTER 1980 REPORT PERIOD.

9/80	SYSTEM	.0	.0	720	0	0	.0
	SYSTEM	73.1	21.2	744	216	158	23.2
	٥	98.1	28.5				
	С	.0	.0				
	В	98.1	28.5				
8/80	A	96.3	27.9				
.,	- · · · · ·						
7/80	SYSTEM			744			

### ** PROBLEMS/SOLUTIONS/COMMENTS

AN EIGHT WEEK BOILER AND FGD SYSTEM SCHEDULED OUTAGE BEGAN DURING THE WEEK OF AUGUST 11. THE FGD SYSTEM WAS EXPECTED TO BE OUT OF SERVICE FOR 8-12 WEEKS. DURING THE OUTAGE THE FOLLOWING REPAIRS WERE TO BE PEPFORMED:

- 1. REPLACE FABRIC EXPANSION JOINTS WITH ELASTOMER JOINTS
- 2. REPLACE GUNITE LININGS ON OUTLET DUCTWORK
- 3. BEGIN RE-LINING SO2 MODULES RUBBER LINING DUE TO SEVERE BLISTERING
- 4. COAT THICKENER OVERFLOW TANK WITH COAL TAR EPOXY
- 5. MISCELLANEOUS PUMP AND VALVE MAINTENANCE
- 6. UPGRADE THE ISOLATION DAMPERS

10/80 SYSTEM .0 .0 744 0 0 .0

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE PLEASANTS 1 FGD SYSTEM REMAINED OFF LINE THROUGH THE MONTH OF OCTOBER.

11/80	SYSTEM	720
12/80	SYSTEM	744

### ** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION FOR THE MONTHS OF NOVEMBER AND DECEMBER WAS NOT AVAILABLE.

1/81	SYSTEM	744	86.2
2/81	SYSTEM	672	81.0
3/81	SYSTEM	744	33.2

### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING AN FGD SYSTEM OUTAGE IN MARCH IT WAS DISCOVERED THAT THE PLASITE LINING IN THE OUTLET DUCTWORK FOR MODULES B AND D WAS FAILING. THE B MODULE DUCTWORK WAS PATCHED AND THE MODULE RETURNED TO SERVICE. THE D MODULE WAS KEPT OFF LINE AND THE OUTLET DUCTWORK FOR THIS MODULE WILL BE RELINED WITH CHLOROBUTYL RUBBER.

4/81	SYSTEM	720
5/81	SYSTEM	744
6/81	SYSTEM	720
10/81	SYSTEM	744
11/81	SYSTEM	720

DEDION	MODUL F	AVAILABILITY	ODED ARTITTY	PERFORMAN	CE DATA	7 DE	MOVAL		BOTI ED		
						S02	PART.	HOURS	HOURS	HOURS	FACTOR
12/81	SYSTEM							744			
	SYSTEM							744			
-	SYSTEM										
	SYSTEM							672			
	SYSTEM							744			
								720			
	SYSTEM							744			
	SYSTEM							720			
	SYSTEM							744			
8/82	SYSTEM							744			
9/82	SYSTEM							720			
10/82	SYSTEM							744			
11/82	SYSTEM							720			
12/82	SYSTEM							744			
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
		I	NFORMATION W	AS UNAVAILABI	LE FOR THE PE	ERIOD	OF APR	IL 198	1 TO DE	CEMBER	1982.
1/83	1A 1B		38.7 90.8		38.4 90.2						
	10		68.2		67.7						
	1D SYSTEM		46.8 81.5		46.5 81.0			744	739	602	74 0
	3131211		01.5		01.0			, , , ,	737	302	, 4.0
2/83			.0		.0						
	1B		99.1		99.1						
	10		100.0 70.7		100.0 70.7						
	1D SYSTEM		89.9		89.9			672	672	604	67.0
	3131211		07.7		٠,,,			٥, ٦	•/-	•••	07.0
3/83	14		39.5		29.4						
	18		64.0		47.7						
	1C		90.8		67.7						
	1D		53.3		39.8			766		450	<b>53.0</b>
	SYSTEM		82.5		61.6			744	<b>5</b> 55	450	51.0
	** PRO	BLEMS/SOLUTIO				_					
		E	XPANSION JOI	NTS WERE REP		JLES 1	A AND	18 DUR	ING MAR	CH.	
4/83	1A		42.8		33.3						
	18		76.8		59.9						
	10		39.0		30.4						
	1D		92.7		72.2						/ <del>-</del> -
	SYSTEM		83.8		65.3			720	561	470	48.0
5/83	1A		83.7		67.7						
2,03	1B		57.1		46.2						
	10		57.6		46.6						
	1D		82.4		66.7						
	SYSTEM		93.6		75.8			744	602	564	54.0
	5.51211							•		•	

MONONGAHELA POWER: PLEASANTS 1 (CONT.)

PERFORMANCE DATA					
PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION	% REMOVAL	PER	BOILER	FGD	CAP.
	SO2 PART	. HOURS	HOURS	HOURS	FACTOR

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING APRIL AND MAY, 1983.

6/83	1A	99.6	33.3
	18	99.2	33.2
	1C	100.0	34.4
	10	.0	.0
	SYSTEM	99.6	33.7

### ** PROBLEMS/SOLUTIONS/COMMENTS

UNIT 1 WAS OUT OF SERVICE DURING PART OF JUNE FOR AN ANNUAL OUTAGE.

LIME SLURRY TANKS WERE LINED WITH EPOXY COATING DURING THE ANNUAL OUTAGE IN JUNE.

720 241 242 24.0

OUTLET DUCTS WERE RELINED DURING THE OUTAGE IN JUNE.

THE MODULE 1D MIST ELIMINATOR SECTION WAS RELINED WITH CHLOROBUTYL RUBBER DURING THE ANNUAL OUTAGE IN JUNE.

7/8	33 SYSTEM	744
8/8	33 SYSTEM	744
9/8	33 SYSTEM	720

### ** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE THIRD QUARTER OF 1983.

10/83	SYSTEM	744
11/83	SYSTEM	720
12/83	SYSTEM	744

### ** PROBLEMS/SOLUTIONS/COMMENTS

### INFORMATION WAS UNAVAILABLE FOR THE FOURTH QUARTER OF 1983.

1/84	SYSTEM	744
2/84	SYSTEM	696
3/84	SYSTEM	744
4/84	SYSTEM	720
5/84	SYSTEM	744
6/84	SYSTEM	720
7/84	SYSTEM	744
8/84	SYSTEM	744
9/84	SYSTEM	720

MONONGAHELA POWER: PLEASANTS 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE FIRST THREE QUARTERS OF 1984.

# SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

MONONGAHELA POWER COMPANY NAME PLEASANTS PLANT NAME UNIT NUMBER WILLOW ISLAND CITY WEST VIRGINIA STATE 21. ( .050 LB/MMBTU) 516. ( 1.200 LB/MMBTU) 301. ( .700 LB/MMBTU) 1160 REGULATORY CLASSIFICATION PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J NET PLANT GENERATING CAPACITY - MW NET PLANT GENERATING CAPACITY - MW
GROSS UNIT GENERATING CAPACITY - MW
NET UNIT GENERATING CAPACITY W/FGD - MW
NET UNIT GENERATING CAPACITY WO/FGD - MW 626 580 595 EQUIVALENT SCRUBBED CAPACITY - MW 626 ** UNIT DATA - BOILER AND STACK FOSTER WHEELER BOILER SUPPLIER PULVERIZED COAL BOILER TYPE BOILER SERVICE LOAD BASE BASE 1132.56 (2400000 ACFM) 132.2 (270 F) 305. (1000 FT) CONCRETE 6.1 (20.0 FT) DESIGN BOILER FLUE GAS FLOW - CU.M/S BOILER FLUE GAS TEMPERATURE - C STACK HEIGHT M STACK HEIGHT M STACK SHELL STACK TOP DIAMETER - M ** FUEL DATA FUEL TYPE COAL FUEL GRADE BITUMINOUS AVERAGE HEAT CONTENT - J/G 29075. ( 12500 BTU/LB) RANGE HEAT CONTENT - BTU/LB 11000-13300 AVERAGE ASH CONTENT - % RANGE ASH CONTENT - % 14.7-16.0 RANGE ASH CONTENT - % 4.50 RANGE MOISTURE CONTENT - % 3.0-5.0 AVERAGE SULFUR CONTENT - % 3.00 2.5-3.5 RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % .05 ***** RANGE CHLORIDE CONTENT - % *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER n TYPF NONE ** FABRIC FILTER NUMBER TYPE NONE ** ESP NUMBER 2 NUMBER OF SPARES O TYPE COLD SIDE AIR CORRECTION DIVISION, UOP SUPPLIER INLET FLUE GAS CAPACITY - CU.M/S
INLET FLUE GAS TEMPERATURE - C 566.3 (1200000 ACFM) 132.2 ( 270 F) PARTICLE REMOVAL EFFICENCY - % 99.5 ** PARTICLE SCRUBBER ñ GENERIC TYPE NONE SPECIFIC TYPE N/A TRADE NAME/COMMON NAME N/A SHELL GENERIC MATERIAL N/A SHELL SPECIFIC MATERIAL N/A LINER GENERIC MATERIAL N/A

N/A

LINER SPECIFIC MATERIAL

### *** FGD SYSTEM

```
** GENERAL DATA
   SALEABLE PRODUCT/THROWAWAY PRODUCT
                                               THROWAWAY PRODUCT
   SO2 REMOVAL MODE
                                               WET SCRUBBING
                                               LIME
   PROCESS TYPE
   PROCESS ADDITIVES
                                               NONE
   SYSTEM SUPPLIER
                                               BABCOCK & WILCOX
   A-E FIRM
                                               UNITED ENGINEERS & CONSTRUCTORS
   DEVELOPMENT LEVEL
                                               FULL SCALE
   NEW/RETROFIT
                                              NEW
   UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.55
   UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                  90.00
   ENERGY CONSUMPTION - %
                                                  2.4
   CURRENT STATUS
                                               1
   COMMERCIAL START-UP
                                               12/80
   INITIAL START-UP
                                               10/80
   CONTRACT AWARDED
                                                9/75
** DESIGN AND OPERATING PARAMETERS
   DESIGN COAL SULFER CONTENT - %
                                                   4.50
   DESIGN COAL HEAT CONTENT - J/G
                                               28842.4
                                                              ( 12400 BTU/LB)
   DESIGN COAL ASH CONTENT - %
                                                 16.00
    DESIGN MOISTURE CONTENT - X
                                                   5.00
   DESIGN CHLORIDE CONTENT - %
                                                    .05
    SPACE REQUIREMENTS - SQ M
                                               20252.2
                                                              ( 218000 SQ FT)
   OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                 208.0
** QUENCHER/PRESATURATOR
   NUMBER
   TYPE
                                               VENTURI
   SUPPLIER
                                               BABCOCK & WILCOX
    INLET GAS FLOW - CU. M/S
                                                 283.14 ( 600000 ACFM)
   INLET GAS TEMPERATURE - C
                                                 148.9
                                                             ( 300 F)
   PRESSURE DROP KPA
                                                  1.0
                                                             ( 4.0 IN-H20)
   LIQUID RECIRCULATION RATE - LITERS/S
                                                 504.
                                                             ( 8000 GPM)
    L/G RATIO
               L/CU. M
                                                              ( 13.3 GAL/1000 ACFM)
                                                   1.8
   CONSTRUCTION MATERIAL GENERIC TYPE
                                              CARBON STEEL
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                              AISI 1110
** ABSORBER
                                                4
   NUMBER
   NUMBER OF SPARES
                                                1
                                               TRAY TOWER
   GENERIC TYPE
                                               SIEVE TRAY
    SPECIFIC TYPE
   TRADE NAME/COMMON TYPE
                                               N/A
    SUPPLIER
                                               BABCOCK & WILCOX
    SHELL GENERIC MATERIAL
                                               CARBON STEEL
    SHELL SPECIFIC MATERIAL
                                               AISI 1110
    SHELL MATERIAL TRADE NAME/COMMON TYPE
                                               N/A
                                               ORGANIC
    LINER GENERIC MATERIAL
                                               NATURAL RUBBER
    LINER SPECIFIC MATERIAL
                                               BLACK NATURAL RUBBER
    LINER MATERIAL TRADE NAME/COMMON TYPE
                                               PERFORATED TRAYS
    GAS CONTACTING DEVICE TYPE
   NUMBER OF CONTACTING ZONES
                                               1
                                                1008.
                                                              (16000 GPM)
    LIQUID RECIRCULATION RATE - LITER/S
    L/G RATIO L/CU.M
                                                  4.0
                                                              ( 30.2 GAL/1000 ACF)
    GAS-SIDE PRESSURE DROP - KPA
                                                   1.2
                                                              ( 5.0 IN-H20)
   SUPERFICAL GAS VELOCITY - M/SEC
                                                   3.0
                                                             ( 10.0 FT/S)
   INLET GAS FLOW - CU. M/S
                                                 250.11
                                                             ( 530000 ACFM)
   INLET GAS TEMPERATURE - C
                                                              ( 125 F)
                                                  51.7
   SO2 REMOVAL EFFICIENCY - %
                                                  90.0
** MIST ELIMINATOR
   PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                               PRIMARY COLLECTOR
   NUMBER PER SYSTEM
                                                4
   NUMBER OF SPARES PER SYSTEM
                                                1
   NUMBER PER MODULE
                                               1
   GENERIC TYPE
                                               IMPINGEMENT
                                               BAFFLE
   SPECIFIC TYPE
```

	TRADE NAME/COMMON TYPE  MANUFACTURER  CONFIGURATION  NUMBER OF STAGES  NUMBER OF PASSES PER STAGE  DISTANCE BETWEEN STAGES - CM  SUPERFICAL GAS VELOCITY - M/S  CONSTRUCTION MATERIAL GENERIC TYPE  CONSTRUCTION MATERIAL SPECIFIC TYPE  WASH WATER SOURCE  WASH FREGUENCY  WASH RATE - L/S	·	(84.0 IN) ( 10.0 FT/S) CED POLYESTER
**	REHEATER NUMBER NUMBER OF SPARES GENERIC TYPE SPECIFIC TYPE TRADE NAME/COMMON TYPE LOCATION PERCENT GAS BYPASSED - AVG TEMPERATURE INCREASE - C INLET FLUE GAS TEMPERATURE - C OUTLET FLUE GAS TEMPERATURE - C CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE	1 0 BYPASS COLD SIDE N/A AHEAD OF STACE 15.0 13.9 51.7 65.6 NR	( 25 F) ( 125 F) ( 150 F)
**	FANS NUMBER NUMBER OF SPARES DESIGN SUPPLIER FUNCTION APPLICATION SERVICE FLUE GAS FLOW RATE - CU.M/S FLUE GAS TEMPERATURE - C PRESSURE DROP - KPA CONSTRUCTION MATERIAL GENERIC TYPE	132.2 7.9	DARD ( 566000 ACFM) ( 270 F) (26.0 IN-H20)
**	FANS NUMBER NUMBER OF SPARES DESIGN SUPPLIER FUNCTION APPLICATION SERVICE FLUE GAS FLOW RATE - CU.M/S FLUE GAS TEMPERATURE - C PRESSURE DROP KPA CONSTRUCTION MATERIAL GENERIC TYPE	132.2	DARD (1045000 ACFM) ( 270 F) (25.0 IN-H20)
**	DAMPERS NUMBER FUNCTION GENERIC TYPE SPECIFIC TYPE MANUFACTURER SERVICE CONDITIONS CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE	FORNEY ENGINE 270 CARBON STEEL	SED BLADE MULTILOUVER ERING LOW ALLOY [HSLA]
**	DAMPERS NUMBER FUNCTION GENERIC TYPE SPECIFIC TYPE MANUFACTURER	4 SHUT-OFF LOUVER PARALLEL/OPPO FORNEY ENGINE	SED BLADE MULTILOUVE ERING

SERVICE CONDITIONS CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE

LINER SPECIFIC MATERIAL TYPE

### ** DUCTWORK

LOCATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE

AISI 1110 NONE LINER SPECIFIC MATERIAL TYPE N/A

# ** DUCTWORK

LOCATION SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE

AISI 1110 ORGANIC; INORGANIC ASPHALT-URETHANE; BOROSILICATE GLASS

** DUCTWORK LOCATION

SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE

** DUCTHORK LOCATION

> SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE

** REAGENT PREPARATION EQUIPMENT FUNCTION DEVICE DEVICE TYPE MANUFACTURER NUMBER

NUMBER OF SPARES PRODUCT QUALITY - % SOLIDS

** TANKS

SERVICE RECIRCULATION ME WASH SLURRY TRANSFER SLURRY FEED THICKENER OVERFLOW SLUDGE STABILIZATION

** PUMPS SERVICE

> QUENCHER RECIRCULATION ABSORBER RECIRCULATION THICKENER UNDERFLOW LIME SLURRY TRANSFER LIME SLURRY FEED SLUDGE TRANSFER RETURN WATER

** SOLIDS CONCENTRATING/DEWATERING

DEVICE NUMBER NUMBER OF SPARES CONFIGURATION DIMENSIONS - FT CAPACITY

OUTLET AFTER BYPASS JUNCTION

CARBON STEEL AISI 1110 INORGANIC

125

NONE

INLET

OUTLET

N/A

STAINLESS STEEL

AUSTENITIC

CARBON STEEL

CARBON STEEL

BYPASS CARBON STEEL AISI 1110 NONE N/A

SLAKER DETENTION N/A DORR-OLIVER 3 15.0

NUMBER

**** **** 1 1 2

NUMBER _____ 8

16 **** 2 **** 4

THICKENER 2

CIRCULAR 175.0 DIA X 10.0

2190000

MONONGAHELA POWER: PLEASANTS 2 (CONT.)

CARBON STEEL SHELL GENERIC MATERIAL TYPE SHELL SPECIFIC MATERIAL TYPE AISI 1110 ORGANIC COAL TAR EPOXY LINER GENERIC MATERIAL TYPE LINER SPECIFIC MATERIAL TYPE ABSORBER BLEED FEED STREAM SOURCE FEED STREAM CHARACTERISTICS 6% SOLIDS 30% SOLIDS [27-32%]; PH 8.0 TO SLUDGE TREATMENT OUTLET STREAM CHARACTERISTICS OUTLET STREAM DISPOSITION OVERFLOW STREAM DISPOSITION RECIRCULATION TANK

*** SALEABLE BYPRODUCTS

NATURE

NONE

### *** SLUDGE

** TREATMENT METHOD DEVICE PROPRIETARY PROCESS

INLET QUALITY - %

** DISPOSAL NATURE

> TYPE LOCATION

SITE TRANSPORTATION METHOD SITE TREATMENT SITE DIMENSIONS

SITE SERVICE LIFE - YRS

** FROCESS CONTROL AND INSTRUMENTATION

PROCESS STREAM CHEMICAL PARAMETERS PHYSICAL VARIABLES CONTROL LEVELS MONITOR TYPE MONITOR LOCATION

** WATER BALANCE WATER LOOP TYPE RECEIVING WATER STREAM SOURCE OF MAKEUP WATER

** CHEMICALS AND CONSUMPTION FUNCTION

NAME PRINCIPAL CONSTITUENT SOURCE/SUPPLIER CONSUMPTION UTILIZATION - % POINT OF ADDITION

** FGD SPARE CAPACITY INDICES

ABSCRBER - % FAN - % SLAKER - % THICKENER - %

** FGD SPARE COMPONENT INDICES

ABSORBER FAN SLAKER THICKENER

FIXATION MIX TANK DRAVO [CALCILOX] 30.0

FINAL POND OFF-SITE [1.5 MILES] PIPELINE NONE 200 ACRES X 200 FT 31

OUTLET FROM ABSORBER PH, 502 DENSITY, FLOW PH 5.9-6.0; 6% SOLIDS IN SLURRY UNILOC [PH], LEAR SIEGLER [SO2], TEXAS NUCLEAR [ ABSORBER DOWNCOMER FOR PH

CLOSED OHIO RIVER

RIVER WATER AND COOLING TOWER BLOWDOWN

ABSORBENT THIOSORBIC LIME >90% CAO, 4-7% MGO DRAVO 11.1 TPH 94.0 SLAKER

33.3

.0 1.0 .0

1.0 . 0

1.0

. 0

6/82 SYSTEM

PERIOD		VAILABILITY OPERABILITY RELIABILITY UTILIZATION		PER	BOILER		
10/80	SYSTEM			744			
	** PROBL	EMS/SOLUTIONS/COMMENTS					
		INITIAL OPERATION OF THE FGD SYSTEM CO	MMENCED IN	LATE O	TOBER :	1980.	
11/80	SYSTEM			720			
12/80	SYSTEM			744			
	** PROBL	EMS/SOLUTIONS/COMMENTS					
		THE UTILITY REPORTED THAT NO MAJOR FGD	PROBLEMS H	AVE BEE	EN ENCO	UNTERE	).
1/81	SYSTEM			744			60.4
	** PROBL	EMS/SOLUTIONS/COMMENTS					
		DURING JANUARY IT WAS NECESSARY TO CLE OVERFLOW TANK AS A RESULT OF PROBLEMS	_				NER
2/81	SYSTEM			672			50.0
	** PROBL	EMS/SOLUTIONS/COMMENTS					
		A NINE-FOOT SECTION OF PIPE HAD TO BE ON MODULE B AS A RESULT OF FAILURE OF			HONTH		
3/81	SYSTEM			744			72.0
	** PROBL	EMS/SOLUTIONS/COMMENTS					
		THE UTILITY REPORTED THAT NO MAJOR FGD DURING MARCH.	-RELATED PR	OBLEMS	WERE E	NCOUNTI	RED
4/81	SYSTEM			720			
5/81	SYSTEM			744			
6/81	SYSTEM			720			
7/81	SYSTEM			744			
8/81	SYSTEM			744			
9/81	SYSTEM			720			
10/81	SYSTEM			744			
11/81	SYSTEM			720			
12/81	SYSTEM			744			
1/82	SYSTEM			744			
2/82	SYSTEM			672			
3/82	SYSTEM			744			
4/82	SYSTEM			744			
5/82	SYSTEM			744			

744

MONONGAHELA POWER: PLEASANTS 2 (CONT.)

7/83 SYSTEM

				PERFORMAN	ICE DATA		m m co us as == ==				
PERIOD	MODULE	AVAILABILITY	OPERABILITY			% REI	MOVAL	PER	BOILER HOURS		CAP. FACTOR
										••••	
7/82	SYSTEM							744			
8/82	SYSTEM							744			
9/82	SYSTEM							720			
10/82	SYSTEM							744			
11/82	SYSTEM							720			
12/82	SYSTEM							744			
		SLEMS/SOLUTIO	NS/COMMENTS								
	1 1.01			C (B)41/47/48/	5 500 THE D		DE 488		. TO DE		1000
		1	NFORMATION WA	3 UNAVAILABL	נ דטא ואב פו	EKTOD (	UF APR	IL 198.	ווי שני	LEMBER	1982.
1/83			76.2		62.0						
	2B		94.9		77.2						
	2C		16.4		13.3						
	2D		100.0		81.7			744	<b>(AF</b>	<b>503</b>	<b>50.0</b>
	SYSTEM		95.8		78.0			744	605	581	58.0
2/83	2A		. 0		.0						
	2B		72.3		72.3						
	2C		99.3		99.3						
	20		99.6		99.6						
	SYSTEM		90.4		90.4			672	`672	607	70.0
3/83	2 A		27.7		27.7						
	2B		90.3		90.3						
	2C		30.6		30.6						
	2D		72.6		72. <b>6</b>						
	SYSTEM		73.7		73.7			744	744	549	70.0
4/83	2 A		98.1		63.5						
	2B		100.0		68.1						
	2C		.0		.0						
	2D		. 0		.0						
	SYSTEM		67.7		43.8			72 <b>0</b>	466	474	35.0
	** PRO	BLEMS/SOLUTIO	NS/COMMENTS								
			THE UNIT 2 STA TO UNIT 1 WAS								ER DUCT
5/83	2A		100.0		99.7						
	2B		65.0		64.7						
	2C		.0		. 0						
	2D		99.2		98.7						
	SYSTEM		88.1		87.7			744	740	652	69.0
6/83	2A		97.9		97.9						
	2B		100.0		100.0						
	2C		63.2		63.2						
	2D		37.2		37.2						
	SYSTEM		99.4		99.4			720	720	716	70.0
	** PRO	BLEMS/SOLUTIO	ONS/COMMENTS								
		7	THE UTILITY RI DURING MAY AND	EPORTED THAT D JUNE, 1983.	NO MAJOR FG	D-RELA	TED PR	OBLEMS	WERE E	NCOUNT	ERED

744

PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION				BOILER HOURS	
8/83	SYSTEM							744		
9/83	SYSTEM							720		
	** PROB	LEMS/SOLUTION	NS/COMMENTS							
		I	NFORMATION WA	AS UNAVAILABL	E FOR THE TH	IRD Q	JARTER	OF 198	33.	
10/83	SYSTEM							744		
11/83	SYSTEM							720		
12/83	SYSTEM							744		
	** PROE	SLEMS/SOLUTION	NS/COMMENTS							
		I	NFORMATION W	AS UNAVAILABL	E FOR THE FO	URTH (	QUARTE	R OF 19	983.	
1/84	SYSTEM							744		
2/84	SYSTEM							696		
3/84	SYSTEM							744		
4/84	SYSTEM							720		
5/84	SYSTEM							744		
6/84	SYSTEM							720		
7/84	SYSTEM							744		
8/84	SYSTEM							744		
9/84	SYSTEM							720		

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE FIRST THREE QUARTERS OF 1984.

# SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

MONTANA POWER COMPANY NAME PLANT NAME UNIT NUMBER COLSTRIP MONTANA STATE 43. ( .100 LB/MMBTU)
516. ( 1.200 LB/MMBTU)
301. ( .700 LB/MMBTU)
664
360
332
344
360 REGULATORY CLASSIFICATION PARTICULATE EMISSION LIMITATION - NG/J SO2 EMISSION LIMITATION - NG/J NOX EMISSION LIMITATION - NG/J HET PLANT GENERATING CAPACITY - MW
GROSS UNIT GENERATING CAPACITY - MW
HET UNIT GENERATING CAPACITY W/FGD - MW
HET UNIT GENERATING CAPACITY WO/FGD - MW HET PLANT GENERATING CAPACITY - MW EQUIVALENT SCRUBBED CAPACITY - MW ** UNIT DATA - BOILER AND STACK COMBUSTION ENGINEERING BOILER SUPPLIER BOILER TYPE PULVERIZED COAL BOILER SERVICE LOAD

BOSIGN BOILER FLUE GAS FLOW - CU.M/S

BOILER FLUE GAS TEMPERATURE - C

STACK HEIGHT M

STACK SHELL

STACK TOP DIAMETER - M

BASE

(1430000 ACFM)

(291 F)

(503 FT)

CONCRETE

5.0

(16.5 FT) ** FUEL DATA FUEL TYPE SUBBITUMINOUS FUEL GRADE 20569. ( 8843 BTU/LB) AVERAGE HEAT CONTENT - J/G RANGE HEAT CONTENT - BTU/LB 8.60 8162-8897 AVERAGE ASH CONTENT - % 6.1-12.6 RANGE ASH CONTENT - % AVERAGE MOISTURE CONTENT - % 23.90 RANGE MOISTURE CONTENT %
AVERAGE SULFUR CONTENT - % 21.0-25.0 0.4-1.0 RANGE SULFUR CONTENT - % AVERAGE CHLORIDE CONTENT - % RANGE CHLORIDE CONTENT - % *** PARTICLE CONTROL ** MECHANICAL COLLECTOR NUMBER Ω TYPE NONE ** ESP NUMBER C TYPE NONE ** PARTICLE SCRUBBER NUMBER NUMBER OF SPARES INITIAL START-UP DATE 9/75 GENERIC TYPE VENTURI TOWER VARIABLE-THROAT/TOP-ENTRY PLUMB BOB SPECIFIC TYPE TRADE NAME/COMMON NAME N/A SUPPLIER THYSSEN/CEA DIMENSIONS ET 15.0 DIA SHELL GENERIC MATERIAL CARBON STEEL SHELL SPECIFIC MATERIAL AISI 1110 INORGANIC LINER GENERIC MATERIAL LINER SPECIFIC MATERIAL PREFIRED BRICK/SHAPES GAS CONTACTING DEVICE TYPE NOHE NUMBER OF CONTACTING ZONES 1 NUMBER OF CONTACTING ZONES LIQUID RECIRCULATION RATE - LITER/S 415.8 ( 6600 GPM) 1.8 (13.8 GAL/1000ACF) L/G RATIO - LITER/CU.M PH CONTROL ADDITIVE LIME/ALKALINE FLY ASH

4.2 (17.0 IN-H20) 61.0 ( 200.0 FT/S)

PRESSUPE DROP KPA

SUPERFICIAL GAS VELOCITY - M/S

```
MONTANA POWER: COLSTRIP 1 (CONT.)
    INLET GAS FLOW RATE - CU.M/S
                                                 225.1
                                                              ( 477000 ACFM)
    INLET GAS TEMPERATURE - C
                                                              ( 291 F)
                                                 143.9
    PARTICLE REMOVAL EFFICIENCY - %
                                                  99.5
*** FGD SYSTEM
 ** GENERAL DATA
    SALEABLE PRODUCT/THROWAWAY PRODUCT
                                               THROWAWAY PRODUCT
    SO2 REMOVAL MODE
                                               WET SCRUBBING
    PROCESS TYPE
                                               LIME/ALKALINE FLYASH
    PROCESS ADDITIVES
                                                NONE
    SYSTEM SUPPLIER
                                                THYSSEN/CEA
    A-E FIRM
                                                BECHTEL
    DEVELOPMENT LEVEL
                                               FULL SCALE
    NEW/RETROFIT
                                               NEM
    UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.50
    UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                 60.00
    ENERGY CONSUMPTION - X
                                                   3.3
     CURRENT STATUS
     COMMERCIAL START-UP
                                                11/75
     INITIAL START-UP
                                                 9/75
     CONTRACT AWARDED
                                                10/72
 ** DESIGN AND OPERATING PARAMETERS
    DESIGN COAL SULFER CONTENT %
                                                   1.00
    DESIGN COAL HEAT CONTENT - J/G
                                                              ( 8162 BTU/LB)
                                               18984.8
    DESIGN COAL ASH CONTENT - %
                                                 12.60
     DESIGN MOISTURE CONTENT - %
                                                  25.00
     DESIGN CHLORIDE CONTENT - %
                                                    .01
     OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                 152.0
 ** QUENCHER/PRESATURATOR
    NUMBER
                                                 0
 ** ABSORBER
     NUMBER
                                                 3
     NUMBER OF SPARES
                                                 ٥
     GENERIC TYPE
                                                COMBINATION TOWER
     SPECIFIC TYPE
                                                VENTURI/SPRAY
     TRADE NAME/COMMON TYPE
                                                N/A
                                                THYSSEN/CEA
     SUPPLIER
     DIMENSIONS - FT
                                                35 DIA X 70.5
     SHELL GENERIC MATERIAL
                                                CARBON STEEL
     SHELL SPECIFIC MATERIAL
                                                AISI 1110
     SHELL MATERIAL TRADE NAME/COMMON TYPE
                                               N/A
     LINER GENERIC MATERIAL
                                                ORGANIC
     LINER SPECIFIC MATERIAL
                                                GLASS FLAKE-FILLED POLYESTER; INERT FLAKE-FILLED
     LINER MATERIAL TRADE NAME/COMMON TYPE
                                                RIGIFLAKE 4850; PLASITE 4020 & 4030
     GAS CONTACTING DEVICE TYPE
                                                VENTURI THROAT AND SPRAY ZONE
     NUMBER OF CONTACTING ZONES
     LIQUID RECIRCULATION RATE - LITER/S
                                                              ( 7600 GPM)
                                                  479.
                                                   2.4
                                                              ( 17.8 GAL/1000 ACF)
     L/G RATIO L/CU.M
     GAS-SIDE PRESSURE DROP - KPA
                                                   4.4
                                                              (17.5 IN-H20)
     SUPERFICAL GAS VELOCITY - M/SEC
                                                    2.7
                                                              ( 9.0 FT/S)
     INLET GAS FLOW - CU. M/S
                                                  201.31
                                                              ( 426600 ACFM)
                                                  48.9
     INLET GAS TEMPERATURE - C
                                                              ( 120 F)
     SO2 REMOVAL EFFICIENCY - %
                                                   80.0
     PARTICLE REMOVAL EFFICENCY - %
                                                   99.5
 ** MIST ELIMINATOR
                                                PRIMARY COLLECTOR
     PRE-MIST ELIMINATOR/MIST ELIMINATOR
     NUMBER PER SYSTEM
                                                 3
     NUMBER OF SPARES PER SYSTEM
                                                 0
     NUMBER PER MODULE
                                                 1
                                                IMPINGEMENT
     GENERIC TYPE
     SPECIFIC TYPE
                                                BAFFLE
```

CLOSED VANE

HORIZONTAL

1

4

HFTI

TRADE NAME/COMMON TYPE

NUMBER OF PASSES PER STAGE

MANUFACTURER

CONFIGURATION

NUMBER OF STAGES

```
MONTANA POWER: COLSTRIP 1 (CONT.)
    FREEBOARD DISTANCE - M
                                                    3.96
                                                             (13.0 FT)
                                                    2.5
    DISTANCE BETWEEN VANES - CM
                                                              ( 1.00 IN)
                                                 120
    VANE ANGLES - DEGREES
     PRESSURE DROP - KPA
                                                    . 1
                                                               ( .3 IN-H20)
                                                    2.7
                                                              ( 8.7 FT/S)
    SUPERFICAL GAS VELOCITY - M/S
                                                ORGANIC
    CONSTRUCTION MATERIAL GENERIC TYPE
                                                POLYPHENYLENE
    CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                BLENDED
    WASH WATER SOURCE
    WASH FREQUENCY
                                                CONTINUOUS UNDERSPRAY AND ONCE/DAY OVERSPRAY
    WASH RATE - L/S
                                                  51.1
                                                             ( 810 GAL/MIN)
 ** REHEATER
    NUMBER
                                                 3
    NUMBER OF SPARES
                                                 0
    NUMBER PER MODULE
                                                 1
    GENERIC TYPE
                                                IN-LINE
     SPECIFIC TYPE
                                                STEAM
     TRADE NAME/COMMON TYPE
                                                PLATECOIL
                                                IN DUCT AFTER ABSORBER
     LOCATION
     PERCENT GAS BYPASSED - AVG
                                                    . 0
     TEMPERATURE INCREASE - C
                                                  30.6
                                                                  55 F)
                                                             ( 426600 ACFM)
     INLET FLUE GAS FLOW RATE - CU. M/S
                                                  201.31
                                                              ( 120 F)
( 175 F)
     INLET FLUE GAS TEMPERATURE - C
                                                  48.9
     CUTLET FLUE GAS TEMPERATURE - C
                                                  79.4
     NUMBER OF HEAT EXCHANGER BANKS
                                                 12
     NUMBER OF BUNDLES PER BANK
                                                 11
     CONSTRUCTION MATERIAL GENERIC TYPE
                                                HIGH ALLOY
                                              NICKEL BASE/CHROMIUM-IRON-COPPER-MOLYBDENUM; NIC
     CONSTRUCTION MATERIAL SPECIFIC TYPE
 ** FANS
    NUMBER
                                                 3
     NUMBER OF SPARES
                                                 Λ
     DESIGN
                                                CENTRIFUGAL
     SUPPLIER
                                                BUFFALO FORGE
     FUNCTION
                                                UNIT
     APPLICATION
                                                INDUCED DRAFT
     SERVICE
                                                DRY
     FLUE GAS FLOW RATE - CU.M/S
                                                 223.21
                                                              ( 473000 ACFM)
                                                               ( 175 F)
     FLUE GAS TEMPERATURE - C
                                                   79.4
     PRESSURE DROP - KPA
                                                   11.0
                                                               (36.0 IN-H20)
     CONSTRUCTION MATERIAL GENERIC TYPE
                                                CARBON STEEL; ORGANIC
 ** DAMPERS
    NUMBER
     FUNCTION
                                                SHUT-OFF
     GENERIC TYPE
                                                BUTTERFLY
     SPECIFIC TYPE
                                                N/A
     MANUFACTURER
                                                ALLIS-CHALMERS
     MODULATION
                                                OPEN/CLOSED
     CONSTRUCTION MATERIAL GENERIC TYPE
                                                CARBON STEEL
     CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                AISI 1110
     LINER GENERIC MATERIAL TYPE
                                                NCNE
     LINER SPECIFIC MATERIAL TYPE
                                                N/A
 ** DAMPERS
     NUMBER
                                                 3
     FUNCTION
                                                SHUT-OFF
     GENERIC TYPE
                                                GUILLOTINE
     SPECIFIC TYPE
                                                SIDE-ENTRY GUILLOTINE
     MANUFACTURER
                                                MOSSER
     MODULATION
                                                OPEN/CLOSED
     CONSTRUCTION MATERIAL GENERIC TYPE
                                                STAINLESS STEEL
     CONSTRUCTION MATERIAL SPECIFIC TYPE
                                                AUSTENITIC
     LINER GENERIC MATERIAL TYPE
                                                NONE
     LINER SPECIFIC MATERIAL TYPE
                                                N/A
 ** DAMPERS
    NUMBER
     FUNCTION
                                                CONTROL
```

LOUVER

PARALLEL BLADE MULTILOUVER

GENERIC TYPE

SPECIFIC TYPE

MANUFACTURER

MODULATION

CONSTRUCTION MATERIAL GENERIC TYPE

CONSTRUCTION MATERIAL SPECIFIC TYPE

LINER GENERIC MATERIAL TYPE

LINER SPECIFIC MATERIAL TYPE

N/A

BUFFALO FORGE

VARIOUS

CARBON STEEL

AISI 1110

NONE

LINER SPECIFIC MATERIAL TYPE

N/A

** DUCTWORK

LOCATION

CONFIGURATION

SHELL GENERIC MATERIAL TYPE

SHELL SPECIFIC MATERIAL TYPE

LINER GENERIC MATERIAL TYPE

LINER SPECIFIC MATERIAL TYPE

INLET
CIRCULAR
CARBON STEEL
AISI 1110
NONE
N/A

** DUCTWORK

LOCATION OUTLET
CONFIGURATION RECTANGULAR
SHELL GENERIC MATERIAL TYPE CARBON STEEL
SHELL SPECIFIC MATERIAL TYPE AISI 1110
LINER GENERIC MATERIAL TYPE ORGANIC
LINER SPECIFIC MATERIAL TYPE GLASS FLAKE-FILLED POLYESTER

** DUCTHORK

LOCATION REHEATER
CONFIGURATION RECTANGULAR
SHELL GENERIC MATERIAL TYPE STAINLESS STEEL
SHELL SPECIFIC MATERIAL TYPE AUSTENITIC
LINER GENERIC MATERIAL TYPE NONE
LINER SPECIFIC MATERIAL TYPE N/A

** REAGENT PREPARATION EQUIPMENT

FUNCTION SLAKER
DEVICE PASTE
MANUFACTURER BIF
NUMBER 2
NUMBER OF SPARES
PRODUCT QUALITY - % SOLIDS 10.0

** TANKS

SERVICE NUMBER

VENTURI & ABSORBER RECYCLE 3
SLURRY TRANSFER 1
SLUPRY STORAGE 1
EFFLUENT BLEED 1
TRAY WASH WATER RECYCLE 1

** PUMPS

SERVICE NUMBER

VENTURI RECIRCULATION 6
ABSORBER RECIRCULATION 6
POND RETURN 3
LIME SYSTEM ****
EFFLUENT BLEED 2
TRAY WASH WATER RECYCLE 2

** SOLIDS CONCENTRATING/DEWATERING

DEVICE NONE

*** SLUDGE

** TREATMENT

METHOD BLEED
DEVICE N/A
PROPRIETARY PROCESS N/A

```
** DISPOSAL
                                               INTERIM
   NATURE
                                               POND
   TYPE
                                               ON-SITE
   LOCATION
   SITE TRANSPORTATION METHOD
                                               PIPELINE
   SITE TREATMENT
                                              CLAY LINING [BENTONITE]
                                                550350 ( 450.0 ACRE-FT)
                                              15 ACRE/20-30 FEET DEEP
    SITE DIMENSIONS
    SITE CAPACITY - CU.M
    SITE SERVICE LIFE - YRS
** DISPOSAL
                                               INTERIM
   NATURE
                                               POND
    TYPE
                                               ON-SITE
    LOCATION
    SITE TRANSPORTATION METHOD
                                               PIPELINE
    SITE TREATMENT
                                               CLAY LINING [BENTONITE]
                                              15 ACRE/20-30 FEET DEEP
    SITE DIMENSIONS
    SITE CAPACITY CU.M
                                                  550350 ( 450.0 ACRE-FT)
    SITE SERVICE LIFE YRS
** DISPOSAL
   NATURE
                                               FINAL
                                               POND
    TYPE
    LOCATION
                                               ON-SITE
    SITE TRANSPORTATION METHOD
                                              PIPELINE
    SITE TREATMENT
                                              CLAY LINING [BENTONITE]
                                              150 ACRE/20-30 FEET DEEP
    SITE DIMENSIONS
    SITE CAPACITY - CU.M
                                                  5503500 ( 4500.0 ACRE-FT)
    SITE SERVICE LIFE - YRS
** PROCESS CONTROL AND INSTRUMENTATION
    PROCESS STREAM
                                               RECIRCULATING SLURRY
    CHEMICAL PARAMETERS
                                               PH
    PHYSICAL VARIABLES
                                               % SOLIDS, FLOW, PRESSURE
    CONTROL LEVELS
                                               PH 4.5 TO 5.5
    MONITOR LOCATION
                                               RECIRCULATION TANK
    PROCESS CONTROL MANNER
                                               MANUAL
    PROCESS CHEMISTRY MODE
                                               FEEDBACK
** WATER BALANCE
    WATER LOOP TYPE
                                               CLOSED
    EVAPORATION WATER LOSS - LITER/S
    EVAPORATION WATER LOSS - LITER/S 0

POND SEEPAGE/RUNOFF WATER LOSS LITERS/S 0

MAKEUP WATER ADDITION - LITERS/S 18.3 ( 290 GPM)

ME WASH, LIME SLAKER, AND SEAL WATER
** CHEMICALS AND CONSUMPTION
    FUNCTION
                                               ABSORBENT
    NAME
                                               LIME/FLY ASH
    PRINCIPAL CONSTITUENT
                                               90% CAO/16-21% CAO AND 5% MGO
    SOURCE/SUPPLIER
                                               PETE LIENE
                                               5 TPD [LIME]
    CONSUMPTION
    POINT OF ADDITION
                                               SLAKER
** FGD SPARE CAPACITY INDICES
    SCRUBBER - %
                                                  20.0
    ABSORBER %
                                                  20.0
    MIST ELIMINATOR - %
                                                    .0
    REHEATER - %
                                                  50.0
    FAN %
                                                  20.0
    SLAKER - %
                                                 100.0
    EFFLUENT HOLD TANK %
                                                  20.0
    RECIRCULATION PUMP - %
                                                  50.0
** FGD SPARE COMPONENT INDICES
    SCRUBBER
                                                     . 5
    ABSOPRED
                                                     . 5
    MIST ELIMINATOR
                                                     . 0
    REHEATER
                                                    . 0
    FAN
```

. 5

SLAKER 1.0
EFFLUENT HOLD TANK .5RECIRCULATION PUMP 1.0

				PERFORMA	NCE DATA	 				
PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION			BOILER HOURS		CAP.
9/75	SYSTEM	.0					720	72		.5
10/75	SYSTEM	.0					744	456		19.4
11/75	SYSTEM	.0					720	576		42.2
12/75	SYSTEM	.0					744	720		59.9
1/76	SYSTEM	90.0					744	672		63.8
2/76	SYSTEM	98.0					696	624		65.4
3/76	SYSTEM	97.6					744	576		57.0
4/76	SYSTEM	74.2					720	672		49.9
5/76	SYSTEM	96.8					744	336		26.0
6/76	SYSTEM	.0			.0		720	0	0	.0
7/76	SYSTEM	93.2					744	480		28.0
8/76	SYSTEM	94.7					744	<b>5</b> 52		37.8
9/76	SYSTEM	88.6					720	720		64.5
10/76	SYSTEM	79.9					744	720		73.1

# ** PROBLEMS/SOLUTIONS/COMMENTS

A TEMPERATURE EXCURSION RESULTED IN DAMAGE TO SYSTEM COMPONENTS CAUSING SYSTEM DOWNTIME.

THE EMERGENCY SCRUBBER QUENCH WATER SUPPLY SYSTEM FAILED TO OPERATE DURING A TEMPERATURE EXCURSION RESULTING IN INTERNAL DAMAGE.

THE LININGS WERE DAMAGED DURING THE OCTOBER TEMPERATURE EXCURSION.

MIST ELIMINATOR DAMAGE OCCURRED AS THE RESULT OF THE TEMPERATURE EXCURSION IN OCTOBER.

11/76	SYSTEM	62.7	720	720	55.6
	** PROBLEMS	S/SOLUTIONS/COMMENTS			
		A FAILURE OF AN ID FAN MOTOR OCCURRED IN NOVEMBER.			

67.2	744	744		73.8	SYSTEM	12/76
72.9	744	744		92.5	SYSTEM	1/77
3.0	48	672		95.4	SYSTEM	2/77
0 .0	0	744	.0	.0	SYSTEM	3/77
49.9	600	720		83.0	SYSTEM	4/77
64.1	624	744		85.4	SYSTEM	5/77
68.6	672	720		87.4	SYSTEM	6/77

MONTANA POWER: COLSTRIP 1 (CONT.)

				PERFORMA	NCE DATA						
PERIOD		AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION	% RE1 SO2	10VAL PART.	PER	BOILER HOURS		CAP. FACTOR
					<b>@ 03 80 80 80 80 80 80 80</b>						
7/77	SYSTEM	85.1				•		744	696		71.8
8/77	SYSTEM	93.3						744			
9/77	SÝSTEM	92.5						720			
10/77	SYSTEM	95.6						744			
11/77	SYSTEM	96.3						720			
12/77	SYSTEM	98.3						744			
1/78	SYSTEM	95.7						744			
2/78	SYSTEM	99.5						672			
3/78	SYSTEM	92.0						744			
4/78	SYSTEM	99.8						720			
5/78	SYSTEM	66.0			1.3			744		10	

# ** PROBLEMS/SOLUTIONS/COMMENTS

THE 66% MAY AVAILABILITY IS BASED UPON 9.92 HOURS OF OPERATION ON TWO SCRUBBERS WHILE THE UNIT WAS BEING BROUGHT BACK ON LINE AFTER COMPLETION OF ITS ANNUAL OVERHAUL.

THE ID FAN MOTOR FOR MODULE 1A WAS NOT AVAILABLE DURING UNIT RESTART IN MAY.

7/78       SYSTEM       95.7       744         8/78       SYSTEM       97.0       744         9/78       SYSTEM       96.0       720         10/78       SYSTEM       95.0       744         11/78       SYSTEM       91.0       720         12/78       SYSTEM       96.7       744         1/79       SYSTEM       97.6       744         2/79       SYSTEM       90.3       672         3/79       SYSTEM       97.3       744         4/79       SYSTEM       98.9       88.4       80.2       720       597         5/79       SYSTEM       99.7       744       744       744         6/79       SYSTEM       99.2       720       597	6/78	SYSTEM	76.0			720	
9/78 SYSTEM 96.0  10/78 SYSTEM 95.0  744  11/78 SYSTEM 91.0  12/78 SYSTEM 96.7  1/79 SYSTEM 97.6  2/79 SYSTEM 90.3  3/79 SYSTEM 97.3  4/79 SYSTEM 98.9  88.4  80.2  720  597  5/79 SYSTEM 89.7	7/ <b>7</b> 8	SYSTEM	95.7			744	
10/78 SYSTEM 95.0 744  11/78 SYSTEM 91.0 720  12/78 SYSTEM 96.7 744  1/79 SYSTEM 97.6 744  2/79 SYSTEM 90.3 672  3/79 SYSTEM 97.3 744  4/79 SYSTEM 98.9 88.4 80.2 720 597  5/79 SYSTEM 89.7 744	8/78	SYSTEM	97.0			744	
11/78 SYSTEM 91.0 720  12/78 SYSTEM 96.7 744  1/79 SYSTEM 97.6 744  2/79 SYSTEM 90.3 672  3/79 SYSTEM 97.3 744  4/79 SYSTEM 98.9 88.4 80.2 720 597  5/79 SYSTEM 89.7 744	9/78	SYSTEM	96.0			720	
12/78       SYSTEM       96.7       744         1/79       SYSTEM       97.6       744         2/79       SYSTEM       90.3       672         3/79       SYSTEM       97.3       744         4/79       SYSTEM       98.9       88.4       80.2       720       597         5/79       SYSTEM       89.7       744       744       744	10/78	SYSTEM	95.0			744	
1/79 SYSTEM 97.6  2/79 SYSTEM 90.3  672  3/79 SYSTEM 97.3  744  4/79 SYSTEM 98.9 88.4  80.2  720 597  5/79 SYSTEM 89.7  744	11/78	SYSTEM	91.0			720	
2/79     SYSTEM     90.3       3/79     SYSTEM     97.3       4/79     SYSTEM     98.9     88.4     80.2     720     597       5/79     SYSTEM     89.7     744	12/78	SYSTEM	96.7			744	
3/79 SYSTEM 97.3 744 4/79 SYSTEM 98.9 88.4 80.2 720 597 5/79 SYSTEM 89.7 744	1/79	SYSTEM	97.6			744	
4/79 SYSTEM 98.9 88.4 80.2 720 597 5/79 SYSTEM 89.7 744	2/79	SYSTEM	90.3			672	
5/79 SYSTEM 89.7 744	3/79	SYSTEM	97.3			744	
	4/79	SYSTEM	98. <b>9</b>	88.4	80.2	720	597
6/79 SYSTEM 95.2 720	5/79	SYSTEM	89.7			744	
	6/79	SYSTEM	95.2			720	

# ** PROBLEMS/SOLUTIONS/COMMENTS

DURING MAY AND JUNE THE UNIT WAS BEING OVERHAULED. THE AVAILABILITY FOR THESE PERIODS IS BASED UPON OPERATIONS BEFORE AND AFTER OVERHAUL.

7/79 SYSTEM 98.0 744

720

MONTANA POWER: COLSTRIP 1 (CONT.)

11/79 SYSTEM

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL SO2 PART. HOURS HOURS FACTOR

8/79 SYSTEM 97.3 744

9/79 SYSTEM 95.2 720

10/79 SYSTEM 92.9 744

## ** PROBLEMS/SOLUTIONS/COMMENTS

97.5

THE ROUTINE MAINTENANCE CAN BE PERFORMED WHILE THE MODULES ARE ON LINE SO THE AVAILABILITY REMAINS HIGH.

12/79	SYSTEM	95.9	744
1/80	SYSTEM	96.5	744
2/80	SYSTEM	97.4	696
3/80	SYSTEM	95.4	744

### ** PROBLEMS/SOLUTIONS/COMMENTS

TOTAL SYSTEM AVAILABILITY CONTINUES TO BE HIGH WITH NO MAJOR FGD SYSTEM PROBLEMS REPORTED DURING THE FIRST QUARTER OF 1980.

4/80 SYSTEM 99.8 720

# ** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR PROBLEMS WITH THE FGD SYSTEM WERE REPORTED BY THE UTILITY DURING APRIL.

5/80 SYSTEM 744

# ** PROBLEMS/SOLUTIONS/COMMENTS

NO AVAILABILITY DATA WERE REPORTED BY THE UTILITY BECAUSE OF A SCHEDULED BOILER AND FGD SYSTEM OUTAGE FOR ROUTINE MAINTENANCE.

6/80 SYSTEM 77.7 720

# ** PROBLEMS/SOLUTIONS/COMMENTS

LOW AVAILABILITY DURING JUNE WAS A RESULT OF THE ANNUAL BOILER AND FGD SYSTEM MAINTENANCE OUTAGE.

7/80 SYSTEM 98.6 744

# ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR PROBLEMS WERE ENCOUNTERED DURING JULY.

8/80 SYSTEM 99.3 744 9/80 SYSTEM 98.3 720

# ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED FOR THE MONTHS OF AUGUST AND SEPTEMBER.

10/80 96.2

PERIOD	MODULE A		Y OPERABILITY RELIABILITY UTILIZATION	% RE	MOVAL	PER			CAP.
	SYSTEM					744			
33.700	3131211	98.2							
11/80	SYSTEM	70.6				720			
12/80	SYSTEM	99.0				744			
	** PROBL	EMS/SOLUT	CONS/COMMENTS						
			THE UTILITY REPORTED NO MAJOR FGD PROB	LEMS I	DURING	THE FO	OURTH Q	UARTER	1980.
1/81	SYSTEM	96.0				744			
2/81	SYSTEM	97.4				672			
	** PROBL	EMS/SOLUT	IONS/COMMENTS						
			DURING JANUARY-FEBRUARY THE UTILITY REPROBLEMS WERE ENCOUNTERED.	PORTE	D THAT	NO MA.	JOR FGD	-RELATE	ED .
3/81	SYSTEM	99.8				744			
4/81	SYSTEM	96.6				720			
5/81	SYSTEM	97.1				744			
6/81	SYSTEM	.0				720		0	
	** PROBL	EMS/SOLUT	IONS/COMMENTS						
			DURING JUNE THE BOILER WAS OUT OF SERVINES TIME ROUTINE PATCHING WAS PERFORM					HAUL.	DURING
7/81	SYSTEM	99.3				744			
8/81	SYSTEM	99.2				744			
9/81	SYSTEM	96.9				720			
	** PROBL	EMS/SOLUT	IONS/COMMENTS						
			DURING THE THIRD QUARTER NO FGD-RELATE	D PRO	BLEMS	WERE E	NCOUNTE	RED.	
10/81	SYSTEM	98.4				744			
11/81	SYSTEM	92.8				720			
12/81	SYSTEM	96.9				744			
	** PROBL	EMS/SOLUT	IONS/COMMENTS						
			DURING THE FOURTH QUARTER THE UTILITY ENCOUNTERED WITH THE FGD SYSTEM.	REPOR	TED TH	ON TA	PROBLEM	S WERE	
1/82	SYSTEM	92.8				744			
2/82	SYSTEM	.0				672			
3/82	SYSTEM	.0				744			

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS FACTOR 

### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING FEBRUARY AND MARCH THE UNIT AND THE FGD SYSTEM WERE TAKEN OFF-LINE FOR AN ANNUAL OVERHAUL.

4/82 SYSTEM 720 5/82 SYSTEM 744

## ** PROBLEMS/SOLUTIONS/COMMENTS

DURING APRIL AND MAY THE UNIT AND FGD SYSTEM WERE OFF-LINE FOR SCHEDULED MAINTENANCE.

6/82	SYSTEM	98.5	720
7/82	SYSTEM	94.2	744
8/82	SYSTEM	91.0	744
9/82	SYSTEM	97.3	720
10/82	SYSTEM	93.8	744
11/82	SYSTEM	89.5	720
12/82	SYSTEM	94.7	744
1/83	SYSTEM	97.5	744
2/83	SYSTEM	96.7	672
3/83	SYSTEM	97.8	744

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE LAST TEN MONTHS OF OPERATION. DURING THIS PERIOD OF TIME THE AVERAGE FGD SYSTEM AVAILABILITY WAS 95.1 PERCENT.

4/83	SYSTEM	87.0	
5/83	SYSTEM	.0	
6/83	SYSTEM	.0	

# ** PROBLEMS/SOLUTIONS/COMMENTS

DURING MAY AND JUNE THE UNIT AND THE FGD SYSTEM WERE TAKEN OFF-LINE FOR A SCHEDULED SPRING OVERHAUL.

744 7/83 SYSTEM

# ** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR THE MONTH OF JULY.

8/83	SYSTEM	95.6	744
9/83	SYSTEM	90.0	720

MONTANA POWER: COLSTRIP 1 (CONT.)

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING AUGUST AND SEPTEMBER.

 10/83
 SYSTEM
 744

 11/83
 SYSTEM
 720

** PROBLEMS/SOLUTIONS/COMMENTS

12/83 SYSTEM

INFORMATION WAS UNAVAILABLE FOR THE FOURTH QUARTER OF 1983.

 1/84
 SYSTEM
 92.9

 2/84
 SYSTEM
 90.6

 3/84
 SYSTEM
 93.9

 744

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED OUTAGES WERE REPORTED DURING THE FIRST QUARTER OF 1984

744

 4/84
 SYSTEM
 98.4

 5/84
 SYSTEM
 96.9

 720

 744

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED OUTAGES WERE REPORTED DURING APRIL AND MAY 1984.

6/84 SYSTEM 720 7/84 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

A SCHEDULED OVERHAUL WAS MADE DURING JUNE AND JULY 1984.

 8/84
 SYSTEM
 744

 9/84
 SYSTEM
 720

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR AUGUST AND SEPTEMBER 1984.

# SECTION 13 DESIGN AND PERFORMANCE DATA FOR OPERATIONAL DOMESTIC FGD SYSTEMS

COMPANY NAME	MONTANA POWER	
PLANT NAME	COLSTRIP	
UNIT NUMBER	2	
CITY	COLSTRIP	
STATE	MONTANA	
REGULATORY CLASSIFICATION	D	
PARTICULATE EMISSION LIMITATION - NG/J	43.	( .100 LB/MMBTU)
SO2 EMISSION LIMITATION - NG/J	516.	( 1.200 LB/MMBTU)
NOX EMISSION LIMITATION - NG/J		( .700 LB/MMBTU)
NET PLANT GENERATING CAPACITY - MW	664	
GROSS UNIT GENERATING CAPACITY - MW	360	
NET UNIT GENERATING CAPACITY W/FGD - MW	332	
NET UNIT GENERATING CAPACITY WO/FGD - MW	344	
EQUIVALENT SCRUBBED CAPACITY - MW	360	
** UNIT DATA - BOILER AND STACK		
BOILER SUPPLIER	COMBUSTION ENG	SINEERING
BOILER TYPE	PULVERIZED COA	<b>L</b>
BOILER SERVICE LOAD	BASE	
DESIGN BOILER FLUE GAS FLOW - CU.M/S	674.82	(1430000 ACFM)
BOILER FLUE GAS TEMPERATURE - C	143.9	( 291 F)
STACK HEIGHT - M	153.	( 503 FT)
STACK SHELL	CONCRETE	
STACK TOP DIAMETER - M	5.0	( 16.5 FT)
** FUEL DATA		
FUEL TYPE	COAL	
FUEL GRADE	SUBBITUMINOUS	
AVERAGE HEAT CONTENT - J/G	20569.	( 8843 BTU/LB)
RANGE HEAT CONTENT - BTU/LB		8162-8897
AVERAGE ASH CONTENT - %	8.60	
RANGE ASH CONTENT - %	6.1-12.6	
AVERAGE MOISTURE CONTENT - %	23.90	
RANGE MOISTURE CONTENT - %	21.0-25.0	
AVERAGE SULFUR CONTENT - %	.78	
RANGE SULFUR CONTENT - X	0.4-1.0	
AVERAGE CHLORIDE CONTENT - %	.01	
RANGE CHLORIDE CONTENT + %	****	
*** PARTICLE CONTROL		
** MECHANICAL COLLECTOR	•	
NUMBER	0 NONE	
TYPE	NUNE	
** ESP		
NUMBER	0	
TYPE	NONE	
TIFE		
** PARTICLE SCRUBBER		
NUMBER	3	
NUMBER OF SPARES	0	
INITIAL START-UP DATE	5/76	
GENERIC TYPE	VENTURI TOWER	
SPECIFIC TYPE	VARIABLE TURO	AT/TOP-ENTRY PLUMB BOB
TRADE NAME/COMMON NAME	A WE TWO FE - LUKOY	
SUPPLIER	N/A	RIVIOP-ENTRY TECHE BOB
		RITTOP-ENTRY TEORID DOD
	N/A Thyssen/cea	KITTOF-ENTRY TEOLOGIS
DIMENSIONS - FT	N/A	KITTOP-ENTRY TEORID DOD
DIMENSIONS - FT SHELL GENERIC MATERIAL	N/A THYSSEN/CEA 15.0 DIA	KITTOP ENTRY TEORID DOD
DIMENSIONS - FT SHELL GENERIC MATERIAL SHELL SPECIFIC MATERIAL	N/A THYSSEN/CEA 15.0 DIA CARBON STEEL	KITTOP ENTRY TEORID DOD
DIMENSIONS - FT SHELL GENERIC MATERIAL SHELL SPECIFIC MATERIAL LINER GENERIC MATERIAL	N/A THYSSEN/CEA 15.0 DIA CARBON STEEL AISI 1110	
DIMENSIONS - FT SHELL GENERIC MATERIAL SHELL SPECIFIC MATERIAL LINER GENERIC MATERIAL LINER SPECIFIC MATERIAL	N/A THYSSEN/CEA 15.0 DIA CARBON STEEL AISI 1110 INORGANIC	
DIMENSIONS - FT SHELL GENERIC MATERIAL SHELL SPECIFIC MATERIAL LINER GENERIC MATERIAL LINER SPECIFIC MATERIAL GAS CONTACTING DEVICE TYPE	N/A THYSSEN/CEA 15.0 DIA CARBON STEEL AISI 1110 INORGANIC PREFIRED BRICE	
DIMENSIONS - FT SHELL GENERIC MATERIAL SHELL SPECIFIC MATERIAL LINER GENERIC MATERIAL LINER SPECIFIC MATERIAL GAS CONTACTING DEVICE TYPE NUMBER OF CONTACTING ZONES	N/A THYSSEN/CEA 15.0 DIA CARBON STEEL AISI 1110 INORGANIC PREFIRED BRICK NONE 1	
DIMENSIONS - FT SHELL GENERIC MATERIAL SHELL SPECIFIC MATERIAL LINER GENERIC MATERIAL LINER SPECIFIC MATERIAL GAS CONTACTING DEVICE TYPE NUMBER OF CONTACTING ZONES LIQUID RECIRCULATION RATE - LITER/S	N/A THYSSEN/CEA 15.0 DIA CARBON STEEL AISI 1110 INORGANIC PREFIRED BRICK NONE 1	K/SHAPES
DIMENSIONS - FT SHELL GENERIC MATERIAL SHELL SPECIFIC MATERIAL LINER GENERIC MATERIAL LINER SPECIFIC MATERIAL GAS CONTACTING DEVICE TYPE NUMBER OF CONTACTING ZONES LIQUID RECIRCULATION RATE - LITER/S L/G RATIO - LITER/CU.M	N/A THYSSEN/CEA 15.0 DIA CARBON STEEL AISI 1110 INORGANIC PREFIRED BRICK NONE 1 415.8	<pre></pre>
DIMENSIONS - FT SHELL GENERIC MATERIAL SHELL SPECIFIC MATERIAL LINER GENERIC MATERIAL LINER SPECIFIC MATERIAL LINER SPECIFIC MATERIAL GAS CONTACTING DEVICE TYPE NUMBER OF CONTACTING ZONES LIQUID RECIRCULATION RATE - LITER/S L/G RATIO - LITER/CU.M PH CONTROL ADDITIVE	N/A THYSSEN/CEA 15.0 DIA CARBON STEEL AISI 1110 INORGANIC PREFIRED BRICK NONE 1 415.8 1.8	<pre></pre>
DIMENSIONS - FT SHELL GENERIC MATERIAL SHELL SPECIFIC MATERIAL LINER GENERIC MATERIAL LINER SPECIFIC MATERIAL GAS CONTACTING DEVICE TYPE NUMBER OF CONTACTING ZONES LIQUID RECIRCULATION RATE - LITER/S L/G RATIO - LITER/CU.M	N/A THYSSEN/CEA 15.0 DIA CARBON STEEL AISI 1110 INORGANIC PREFIRED BRICK NONE 1 415.8 1.8 LIME/ALKALINE	<pre></pre>

```
225.1 ( 477000 ACFM)
143.9 ( 291 F)
    INLET GAS FLOW RATE - CU.M/S
    INLET GAS TEMPERATURE - C
                                                   99.5
    PARTICLE REMOVAL EFFICIENCY - %
*** FGD SYSTEM
** GENERAL DATA
    SALEABLE PRODUCT/THROWAWAY PRODUCT
                                                THROWAWAY PRODUCT
                                                WET SCRUBBING
    SO2 REMOVAL MODE
    PROCESS TYPE
                                                LIME/ALKALINE FLYASH
                                                NONE
    FROCESS ADDITIVES
    SYSTEM SUPPLIER
                                                THYSSEN/CEA
                                                BECHTEL
    A-E FIRM
    DEVELOPMENT LEVEL
                                                FULL SCALE
    NEW/RETROFIT
                                                NFW
    UNIT DESIGN PARTICLE REMOVAL EFFICIENCY - % 99.50
    UNIT DESIGN SO2 REMOVAL EFFICIENCY - %
                                                   60.00
    ENERGY CONSUMPTION - %
    CURRENT STATUS
                                                 1
    COMMERCIAL START-UP
                                                10/76
    INITIAL START-UP
                                                 5/76
    CONTRACT AWARDED
                                                10/72
 ** DESIGN AND OPERATING PARAMETERS
    DESIGN COAL SULFER CONTENT - %
                                                  1.00
     DESIGN COAL HEAT CONTENT - J/G
                                                18984.8
                                                              ( 8162 BTU/LB)
    DESIGN COAL ASH CONTENT - %
DESIGN MOISTURE CONTENT - %
                                                 12.60
                                                  25.00
    DESIGN CHLORIDE CONTENT - X
                                                     .01
    OPER. & MAINT. REQUIREMENT - MANHR/DAY
                                                 152.0
 ** QUENCHER/PRESATURATOR
    NUMBER
 ** ABSORBER
    NUMBER
                                                 3
     NUMBER OF SPARES
                                                 n
                                                COMBINATION TOWER
    GENERIC TYPE
     SPECIFIC TYPE
                                                VENTURI/SPRAY
     TRADE NAME/COMMON TYPE
                                                N/A
     SUPPLIER
                                                THYSSEN/CEA
     DIMENSIONS - FT
                                                35 DIA X 70.5
     SHELL GENERIC MATERIAL
                                                CARBON STEEL
     SHELL SPECIFIC MATERIAL
                                                AISI 1110
     SHELL MATERIAL TRADE NAME/COMMON TYPE
                                                N/A
     LINER GENERIC MATERIAL
                                                ORGANIC
     LINER SPECIFIC MATERIAL
                                                GLASS FLAKE-FILLED POLYESTER; INERT FLAKE-FILLED
     LINER MATERIAL TRADE NAME/COMMON TYPE
                                                RIGIFLAKE 4850; PLASITE 4020 & 4030
     GAS CONTACTING DEVICE TYPE
                                                VENTURI THROAT AND SPRAY ZONE
     NUMBER OF CONTACTING ZONES
                                                2
                                                479.
2.4
     LIQUID RECIRCULATION RATE - LITER/S
                                                               ( 7600 GPM)
     L/G RATIO - L/CU.M
                                                             ( 17.8 GAL/1000 ACF)
     GAS-SIDE PRESSURE DROP - KPA
                                                  4.4
2.7
                                                              (17.5 IN-H2O)
                                                              ( 9.0 FT/S)
( 426600 ACFM)
     SUPERFICAL GAS VELOCITY - M/SEC
     INLET GAS FLOW - CU. M/S
                                                  201.31
     INLET GAS TEMPERATURE - C
                                                              ( 120 F)
                                                  48.9
     SO2 REMOVAL EFFICIENCY - X
                                                  80.0
     PARTICLE REMOVAL EFFICENCY - X
                                                   99.5
 ** MIST ELIMINATOR
     PRE-MIST ELIMINATOR/MIST ELIMINATOR
                                                PRIMARY COLLECTOR
     NUMBER PER SYSTEM
                                                 3
     NUMBER OF SPARES PER SYSTEM
                                                 0
     NUMBER PER MODULE
                                                 1
     GENERIC TYPE
                                                IMPINGEMENT
     SPECIFIC TYPE
                                                BAFFLE
     TRADE NAME/COMMON TYPE
                                                CLOSED VANE
     MANUFACTURER
                                                HEIL
     CONFIGURATION
                                                HORIZONTAL
     NUMBER OF STAGES
                                                    1
     NUMBER OF PASSES PER STAGE
                                                    4
```

#### MONTANA POWER: COLSTRIP 2 (CONT.) FREEBOARD DISTANCE - M 3.96 (13.0 FT) DISTANCE BETWEEN VANES - CM ( 1.00 IN) 2.5 VANE ANGLES - DEGREES 120 PRESSURE DROP - KPA ( .3 IN-H20) SUPERFICAL GAS VELOCITY - M/S 2.7 ( 8.7 FT/S) CONSTRUCTION MATERIAL GENERIC TYPE ORGANIC CONSTRUCTION MATERIAL SPECIFIC TYPE POLYPHENYLENE WASH WATER SOURCE BLENDED WASH FREQUENCY CONTINUOUS UNDERSPRAY AND ONCE/DAY OVERSPRAY WASH RATE - L/S 51.1 ( 810 GAL/MIN) ** REHEATER NUMBER 3 NUMBER OF SPARES Ω NUMBER PER MODULE 1 GENERIC TYPE IN-LINE SPECIFIC TYPE STEAM TRADE NAME/COMMON TYPE PLATECOTI LOCATION IN DUCT AFTER ABSORBER PERCENT GAS BYPASSED - AVG . 0 TEMPERATURE INCREASE - C 30.6 ( 55 F) INLET FLUE GAS FLOW RATE - CU. M/S ( 426600 ACFM) 201.31 ( 120 F) ( 175 F) INLET FLUE GAS TEMPERATURE - C 48.9 OUTLET FLUE GAS TEMPERATURE - C 79.4 NUMBER OF HEAT EXCHANGER BANKS 12 NUMBER OF BUNDLES PER BANK 11 CONSTRUCTION MATERIAL GENERIC TYPE HIGH ALLOY CONSTRUCTION MATERIAL SPECIFIC TYPE NICKEL BASE/CHROMIUM-IRON-COPPER-MOLYBDENUM; NIC ** FANS NUMBER 3 NUMBER OF SPARES 0 DESIGN CENTRIFUGAL SUPPLIER **BUFFALO FORGE FUNCTION** UNIT **APPLICATION** INDUCED DRAFT SERVICE DRY FLUE GAS FLOW RATE - CU.M/S ( 473000 ACFM) 223.21 ( 175 F) FLUE GAS TEMPERATURE - C 79.4 (36.0 IN-H20) PRESSURE DROP - KPA 11.0 CONSTRUCTION MATERIAL GENERIC TYPE CARBON STEEL; ORGANIC ** DAMPERS NUMBER SHUT-OFF **FUNCTION** GENERIC TYPE BUTTERFLY SPECIFIC TYPE N/A ALLIS-CHALMERS MANUFACTURER OPEN/CLOSED MODULATION CARBON STEEL CONSTRUCTION MATERIAL GENERIC TYPE CONSTRUCTION MATERIAL SPECIFIC TYPE AISI 1110 LINER GENERIC MATERIAL TYPE NONE N/A LINER SPECIFIC MATERIAL TYPE ** DAMPERS NUMBER 3 SHUT-OFF FUNCTION GUILLOTINE GENERIC TYPE SIDE-ENTRY GUILLOTINE SPECIFIC TYPE MANUFACTURER MOSSER OPEN/CLOSED MODULATION CONSTRUCTION MATERIAL GENERIC TYPE STAINLESS STEEL AUSTENITIC CONSTRUCTION MATERIAL SPECIFIC TYPE LINER GENERIC MATERIAL TYPE NONE LINER SPECIFIC MATERIAL TYPE N/A ** DAMPERS NIMPED CONTROL

PARALLEL BLADE MULTILOUVER

FUNCTION GENERIC TYPE

SPECIFIC TYPE

MONTANA POWER: COLSTRIP 2 (CONT.)

MANUFACTURER

MODULATION

CONSTRUCTION MATERIAL GENERIC TYPE

CONSTRUCTION MATERIAL SPECIFIC TYPE

LINER GENERIC MATERIAL TYPE

LINER SPECIFIC MATERIAL TYPE

NONE

N/A

** DUCTWORK

LOCATION
CONFIGURATION
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

INLET CIRCULAR CARBON STEEL AISI 1110 NONE N/A

** DUCTWORK

LOCATION

CONFIGURATION
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

OUTLET
RECTANGULAR
CARBON STEEL
AISI 1110
ORGANIC
GLASS FLAKE-FILLED POLYESTER

** DUCTWORK

LOCATION
CONFIGURATION
SHELL GENERIC MATERIAL TYPE
SHELL SPECIFIC MATERIAL TYPE
LINER GENERIC MATERIAL TYPE
LINER SPECIFIC MATERIAL TYPE

REHEATER
RECTANGULAR
STAINLESS STEEL
AUSTENITIC
NONE
N/A

SLAKER

PASTE

10.0

BIF

2

1

** REAGENT PREPARATION EQUIPMENT

FUNCTION
DEVICE
MANUFACTURER
NUMBER
NUMBER OF SPARES
PRODUCT QUALITY - % SOLIDS

** TANKS

SERVICE NUMBER
----VENTURI & ABSORBER RECYCLE
SLURRY TRANSFER
SLURRY STORAGE
EFFLUENT BLEED
TRAY WASH WATER RECYCLE
1

** PUMPS

** SOLIDS CONCENTRATING/DEWATERING

DEVICE

*** SLUDGE

** TREATMENT

METHOD
DEVICE
PROPRIETARY PROCESS
N/A
N/A

**	DISPOSAL NATURE TYPE LOCATION SITE TRANSPORTATION METHOD SITE TREATMENT SITE DIMENSIONS SITE CAPACITY - CU.M SITE SERVICE LIFE - YRS	INTERIM POND ON-SITE PIPELINE CLAY LINING [BENTONITE] 15 ACRE/20-30 FEET DEEP 550350 ( 450.0 ACRE-FT) 3
**	DISPOSAL NATURE TYPE LOCATION SITE TRANSPORTATION METHOD SITE TREATMENT SITE DIMENSIONS SITE CAPACITY - CU.M SITE SERVICE LIFE - YRS	INTERIM POND ON-SITE PIPELINE CLAY LINING [BENTONITE] 15 ACRE/20-30 FEET DEEP 550350 ( 450.0 ACRE-FT) 3
**	DISPOSAL NATURE TYPE LOCATION SITE TRANSPORTATION METHOD SITE TREATMENT SITE DIMENSIONS SITE CAPACITY - CU.M SITE SERVICE LIFE - YRS	FINAL POND ON-SITE PIPELINE CLAY LINING [BENTONITE] 150 ACRE/20-30 FEET DEEP 5503500 ( 4500.0 ACRE-FT) 10
**	PROCESS CONTROL AND INSTRUMENTATION PROCESS STREAM CHEMICAL PARAMETERS PHYSICAL VARIABLES CONTROL LEVELS MONITOR LOCATION PROCESS CONTROL MANNER PROCESS CHEMISTRY MODE	RECIRCULATING SLURRY PH % SOLIDS, FLOW, PRESSURE PH 4.5 TO 5.5 RECIRCULATION TANK MANUAL FEEDBACK
**	WATER BALANCE WATER LOOP TYPE EVAPORATION WATER LOSS - LITER/S POND SEEPAGE/RUNOFF WATER LOSS - LITERS/S MAKEUP WATER ADDITION - LITERS/S SOURCE OF MAKEUP WATER	CLOSED 1.9 ( 30 GPM) 0 18.3 ( 290 GPM) ME WASH, LIME SLAKER, AND SEAL WATER
**	CHEMICALS AND CONSUMPTION FUNCTION NAME PRINCIPAL CONSTITUENT SOURCE/SUPPLIER CONSUMPTION POINT OF ADDITION	ABSORBENT LIME/FLY ASH 90% CAO/16-21% CAO AND 5% MGO PETE LIENE 5 TPD [LIME] SLAKER
**	FGD SPARE CAPACITY INDICES SCRUEBER - % ABSORBER - % MIST ELIMINATOR - % REHEATER - % FAN % SLAKER - % EFFLUENT HOLD TANK - % RECIRCULATION PUMP - %	20.0 20.0 .0 50.0 20.0 100.0 20.0 50.0
**	FGD SPARE COMPONENT INDICES SCRUEBER ABSOPEER MIST ELIMINATOR REHEATER FAN	.5 .5 .0 .0

MONTANA POWER: COLSTRIP 2 (CONT.)

SLAKER 1.0
EFFLUENT HOLD TANK .5
RECIRCULATION PUMP 1.0

				PERFORMAN	ICE DATA	 			 
PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION			BOILER HOURS	CAP. FACTOR
			**********						 
5/76	SYSTEM	100.0					744	72	1.3
6/76	SYSTEM	99.7					720	384	23.2
7/76	SYSTEM	98.7					744	312	19.5
8/76	SYSTEM	95.8					744	240	13.0
9/76	SYSTEM	98.3					720	720	64.6
10/76	SYSTEM	90.3					744	744	77.0
11/76	SYSTEM	94.1					720	720	79.7
12/76	SYSTEM	92.5					744	744	82.3
1/77	SYSTEM	83.4					744	720	68.2
2/77	SYSTEM	93.8					672	648	75.3
3/77	SYSTEM	96.7					744	672	71.3
4/77	SYSTEM	84.5					720	696	68.2
5/77	SYSTEM	63.0					744	312	23.3
6/77	SYSTEM	87.8					720	672	61.4
7/77	SYSTEM	90.6					744	672	57.5
8/77	SYSTEM	81.0					744		
9/77	SYSTEM	89.8					720		
10/77	SYSTEM	77.0					744		

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE 77% OCTOBER AVAILABILITY FOR THIS SYSTEM INCLUDES NON-AVAILABLE HOURS DURING A BOILER OUTAGE. SCRUEBER MAINTENANCE WAS PERFORMED FOR PART OF THIS OUTAGE TIME. THE FIGURE COMES TO 98.1% WHEN THE BOILER OUTAGE OUTAGE TIME IS EXCLUDED FROM THE AVERAGING PERIOD.

11/77	SYSTEM	98.0	720
12/77	SYSTEM	98.4	744
1/78	SYSTEM	97.3	744
2/78	SYSTEM	94.5	672
3/78	SYSTEM	89.1	744

# ** PROBLEMS/SOLUTIONS/COMMENTS

THE BOILER WAS SHUT DOWN FOR AN ANNUAL OVERHAUL ON APRIL 18.

THE UTILITY REPORTED AN AVAILABILITY OF 89.1% FOR MARCH BASED ON 17 DAYS OF OPERATION BEFORE THE UNIT SHUTDOWN FOR THE ANNUAL BOILER OVERHAUL. IF THE SCRUBBING SYSTEM IS ASSUMED TO BE AVAILABLE, I.E. NOT UNDERGOING MAJOR

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

REPAIRS DURING THE BOILER OVERHAUL, THE AVAILABILITY COMES TO 93.8%.

4/78 SYSTEM 86.9

720

# ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED AN AVAILABILITY OF 86.9% FOR APRIL BASED ON EIGHT DAYS OF OPERATION AFTER THE UNIT SHUTDOWN FOR THE ANNUAL BOILER OVERHAUL. IF THE SCRUBBING SYSTEM IS ASSUMED TO BE AVAILABLE, I.E. NOT UNDERGOING MAJOR REPAIRS DURING THE BOILER OVERHAUL, THE AVAILABILITY COMES TO 96.5%.

5/78	SYSTEM	99.1		744		
6/78	SYSTEM	97.4		720		
7/78	SYSTEM	96.4		744		
8/78	SYSTEM	99.0	.0 .	744	0	0
9/78	SYSTEM	94.0	.0	720	0	0
10/78	SYSTEM	99.0	.0	744	0	0
11/78	SYSTEM	99.0	.0	72 <b>0</b>	0	0
12/78	SYSTEM	91.2		744		
1/79	SYSTEM	94.3		744		
2/79	SYSTEM	98.3		672		
3/79	SYSTEM	94.3		744		
4/79	SYSTEM	100.0		720		

# ** PROBLEMS/SOLUTIONS/COMMENTS

DURING APRIL THE UNIT WAS BEING OVERHAULED. THE AVAILABILITY FOR THIS TIME IS BASED UPON OPERATIONS BEFORE AND AFTER THE OVERHAUL.

5/79	SYSTEM	94.4	744
6/79	SYSTEM	98.4	720
7/79	SYSTEM	96.4	744
8/79	SYSTEM	99.3	744
9/79	SYSTEM	92.3	720
10/79	SYSTEM	92.9	744
11/79	SYSTEM	98.4	72 <b>0</b>

# ** PROBLEMS/SOLUTIONS/COMMENTS

THE ROUTINE MAINTENANCE CAN BE PERFORMED WHILE THE MODULES ARE ON LINE SO THE AVAILABILITY REMAINS HIGH.

95.8	8	744
92.7	7	744
98.1	1 6	96

MONTANA POWER: COLSTRIP 2 (CONT.)

-----PERFORMANCE DATA------PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP. SO2 PART. HOURS HOURS FACTOR

3/80 SYSTEM 98.2 744

** PROBLEMS/SOLUTIONS/COMMENTS

TOTAL FGD SYSTEM AVAILABILITY CONTINUES TO BE HIGH WITH NO MAJOR PROBLEMS REPORTED FOR THE FIRST QUARTER OF 1980.

4/80 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

NO AVAILABILITY DATA WERE REPORTED BY THE UTILITY BECAUSE OF A BOILER AND FGD SYSTEM OUTAGE THAT WAS SCHEDULED FOR ROUTINE MAINTENANCE.

5/80 SYSTEM 93.5

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR PROBLEMS WITH THE FGD SYSTEM WERE REPORTED BY THE UTILITY DURING MAY.

6/80 SYSTEM 96.0 720

7/80 SYSTEM 99.7 744

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR PROBLEMS WERE ENCOUNTERED DURING THE JUNE-JULY PERIOD.

8/80 SYSTEM 96.2 744

9/80 SYSTEM 90.5 720

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE MONTHS OF AUGUST AND SEPTEMBER.

10/80 96.0 SYSTEM 744 11/80 96.1 SYSTEM 720

12/80 92.4 SYSTEM 744

** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED NO MAJOR FGD PROBLEMS DURING THE FOURTH QUARTER 1980.

1/81 SYSTEM 97.5 744 2/81 SYSTEM 97.4

** PROBLEMS/SOLUTIONS/COMMENTS

DURING JANUARY AND FEBRUARY NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED.

672

3/81 SYSTEM 98.0 744 4/81 SYSTEM 94.5 720 5/81 SYSTEM . 0 744

PERFORMANCE DATA								
PERIOD MODULE AVAILABILITY								
								FACTOR

# ** PROBLEMS/SOLUTIONS/COMMENTS

DURING MAY THE BOILER WAS OUT OF SERVICE FOR A SCHEDULED OVERHAUL. DURING THIS TIME ROUTINE PATCHING WAS PERFORMED ON THE FGD SYSTEM.

6	/81	SYSTEM	99.3	720
7	/81	SYSTEM	98.4	744
8	/81	SYSTEM	96.7	744
9	/81	SYSTEM	94.2	720

## ** PROBLEMS/SOLUTIONS/COMMENTS

DURING MAY THE BOILER WAS OUT OF SERVICE FOR A SCHEDULED OVERHAUL. DURING DURING THE THIRD QUARTER NO FGD-RELATED PROBLEMS WERE ENCOUNTERED.

10/81	SYSTEM	98.0	744
11/81	SYSTEM	92.6	720
12/81	SYSTEM	96.1	744

# ** PROBLEMS/SOLUTIONS/COMMENTS

DURING THE FOURTH QUARTER THE UTILITY REPORTED THAT NO PROBLEMS WERE ENCOUNTERED WITH THE FGD SYSTEM.

1/82	SYSTEM	92.5	744
2/82	SYSTEM	93.1	672
3/82	SYSTEM		744

### ** PROBLEMS/SOLUTIONS/COMMENTS

DURING MARCH THE UNIT AND THE FGD SYSTEM WERE TAKEN OUT OF SERVICE FOR AN ANNUAL OVERHAUL.

4/82	SYSTEM	96.7	720
5/82	SYSTEM	94.9	744

# ** PROBLEMS/SOLUTIONS/COMMENTS

DURING APRIL AND MAY THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE EXPERIENCED.

6/82	SYSTEM	90.0	720
7/82	SYSTEM	95.0	744
8/82	SYSTEM	97.8	744
9/82	SYSTEM	96.0	720
10/82	SYSTEM	96.2	744
11/82	SYSTEM	93.4	720
12/82	SYSTEM	97.0	744

MONTANA POWER: COLSTRIP 2 (CONT.)

				PERFORMAI	NCE DATA	 		 	
PERIOD	MODULE	AVAILABILITY	OPERABILITY	RELIABILITY	UTILIZATION				CAP. FACTOR
1/83	SYSTEM	94.8					744		
2/83	SYSTEM	99.9					672		
3/83	SYSTEM						744		

## ** PROBLEMS/SOLUTIONS/COMMENTS

THE UTILITY REPORTED THAT NO FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE LAST SEVEN MONTHS OF OPERATION. DURING THIS PERIOD OF TIME THE AVERAGE FGD SYSTEM AVAILABILITY WAS 95.1 PERCENT.

THE UTILITY REPORTED THAT NO FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE FIRST QUARTER 1983. THE UNIT WAS SHUTDOWN IN MARCH FOR A SCHEDULED YEARLY SPRING OVERHAUL.

83 SYSTEM .0	
783 SYSTEM 98.4	
'83 SYSTEM 99.1	

### ** PROBLEMS/SOLUTIONS/COMMENTS

THE SPRING OVERHAUL ENDED IN APRIL AND THE UNIT AND FGD SYSTEM WERE PLACED BACK INTO SERVICE. THE UTILITY REPORTED THAT NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING THE REMAINDER OF THE SECOND QUARTER.

7/83 SYSTEM 744

# ** PROBLEMS/SOLUTIONS/COMMENTS

# INFORMATION WAS UNAVAILABLE FOR THE MONTH OF JULY.

8/83	SYSTEM	97.1	744
9/83	SYSTEM	97.0	720

# ** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE ENCOUNTERED DURING AUGUST AND SEPTEMBER.

10/83 SYSTEM	744
11/83 SYSTEM	720
12/83 SYSTEM	744

### ** PROBLEMS/SOLUTIONS/COMMENTS

# INFORMATION WAS UNAVAILABLE FOR THE FOURTH QUARTER OF 1983.

1/84	SYSTEM	90.4	744
2/84	SYSTEM	97.0	696
3/84	SYSTEM	95.1	744

PERIOD MODULE AVAILABILITY OPERABILITY RELIABILITY UTILIZATION % REMOVAL PER BOILER FGD CAP.

SO2 PART. HOURS HOURS FACTOR

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED OUTAGES WERE REPORTED DURING THE FIRST QUARTER OF 1984

4/84 SYSTEM 720

5/84 SYSTEM 744 6/84 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

A SCHEDULED OVERHAUL WAS MADE DURING THE ENTIRE SECOND QUARTER OF 1984.

7/84 SYSTEM 100.0 744

** PROBLEMS/SOLUTIONS/COMMENTS

NO MAJOR FGD-RELATED PROBLEMS WERE REPORTED DURING JULY.

8/84 SYSTEM 744

9/84 SYSTEM 720

** PROBLEMS/SOLUTIONS/COMMENTS

INFORMATION WAS UNAVAILABLE FOR AUGUST AND SEPTEMBER 1984.

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16 ABSTRACT

This report, which is generated by a computerized data base system, represents a survey of operational and planned domestic utility flue gas desulfurization (FGD) system. The three volume set summarizes information contributed by the utility industry, system and equipment suppliers, system designers, research organizations, and regulatory agencies. The data cover system design, fuel characteristics, operating history, and actual system performance. Also included is a unit-by-unit discussion of problems and solutions associated with the boilers, scrubbers, and FGD systems.

The development status (operational, under construction, or in the planning stages), system supplier, process, waste disposal practice, and regulatory class are tabulated alphabetically by utility company. Simplified process flow diagrams of FGD systems, definitions, and a glossary of terms are attached to the report. Current data for domestic FGD systems show 124 systems in operation, 25 systems under construction, and 68 systems planned. The current FGD-controlled capacity in the United States is 47,255 MW.

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