ENFORCEMENT WORKSHOP ON PLANT INSPECTION AND EVALUATION PROCEDURES

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PERFORMANCE EVALUATION



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ENFORCEMENT WORKSHOP ON PLANT INSPECTION AND EVALUATION

COUNTERFLOW INSPECTION PROCEDURES FOR PERFORMANCE BASELINE ASSESSMENT AND ROUTINE EVALUATION

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SECTION 1

COUNTERFLOW INSPECTION PROCEDURES FOR PERFORMANCE BASELINE ASSESSMENT AND ROUTINE EVALUATION

The Counterflow Inspection Procedure has been developed by PEDCo Environmental to aid both the source operators and regulatory agency inspectors to routinely evaluate air pollution control equipment performance. The fundamental principal of the Counterflow Techniques is simply that performance diaggnosis is done by comparison of observed operating conditions with a site-specific baseline operating condition. It is recognized that field measurements are sometimes subject to error or impossible; therefore, diagnosis is based on sets of trends rather than just one parameter. Even when some of the basic data is missing, it is still possible to reach meaningful and accurate conclusions.

The purpose of the Counterflow Technique is to rapidly identify significant changes in performance and the possible reasons for the changes. It does not, necessarily, provide definite evidence of noncompliance nor does it, necessarily provide a specific list of repairs required.

Persons utilizing the Counterflow Inspection Technique should have a technical background--preferably engineering experience. As with any work involving equipment, care should be exercised. Section 6 provides some minimum guidelines and should be read and reread regularly. Formal safety training is highly recommended for this activity and any field work involving air pollution control equipment.

No single technique can satisfy all source characteristics and inspection circumstances. Inspectors and source operators should modify these procedures whenever necessary.

1.1 BASELINE ASSESSMENT

Baseline determinations are preferably done soon after the unit is installed and the shakedown period has been successfully completed. For existing units, an adequate baseline can be developed during a properly conducted stack test. The purpose of the baseline assessment is to provide a sitespecific comparison of equipment performance.

The inspection procedures (and forms) presented in this report should be used for both the baseline assessment and the routine evaluation. There are several additional items, however, that should be accomplished, namely:

- Request a set of general arrangement drawings of the control equipment, ventilation system layout, and waste handling system;
- Evaluate the stack test location and procedures to ensure the emissions data will be accurate and complete;
- 3. Carefully describe all internal conditions (if such inspections can be conducted safely). Photographs are extremely valuable and should be taken if it is safe to do so and if plant personnel permits;
- 4. The sounds of operating components, such as rappers and solenoids, should be noted so that the inspector will be able distinguish developing problems;
- 5. Obtain a complete set of process operating conditions, fan characteristics, and raw material characteristics; and
- 6. Obtain Method 9 opacity readings.

Using the opacity observation and the stack test results, the inspector should evaluate how close the source is operating to the applicable regulations. If the margin is small, the variability is normal; performance may be enough to result in frequent violations. If the source is initially well-below the standard, major changes in operation or severe deterioration of control equipment is needed to result

in noncompliance. The inspector must <u>always</u> be congnizant of the compliance margin. The Counterflow Inspection Procedures are used to evaluate the significance of the changes since the baseline assessment.

SECTION 2

COUNTERFLOW INSPECTION CONCEPTS

Proceeding counter to the gas flow (backward through the system) should minimize inspection time and reporting requirements and maximize the amount of useful information obtained. More specifically, the information on effluents and control equipment gained early in the inspection is not only the easiest to obtain, it can be used later either to narrow the scope of the inspection or to terminate the inspection without completing the most time-consuming part of the evaluation--namely, the process equipment.

As shown in the list below, the steps start at the stack, proceed backward through the system, and end with the process equipment. For regulatory agency personnel, there are some additional preinspection and post-inspection steps required.

Counterflow Inspection Procedure

Observe the stack effluent
Check the continuous monitor(s)
Measure the fan parameters and evaluate physical
condition
Analyze the control equipment performance and
physical conditions
Check the ventilation system performance and
physical condition
Evaluate process operating conditions
Check raw materials and/or fuels

Pre-inspection Steps (regulatory agency personnel only)

Review the source files Schedule the inspection Check the inspection equipment Observe the plant surroundings Request entry to the plant Interview plant official(s)

Post-inspection Steps (regulatory agency personnel only)

Interview plant official(s)
Update source files
Prepare report

SECTION 3

PRE-INSPECTION

3.1 FILE REVIEW

A logical starting point for Agency inspectors is to review the files concerning the specific plant. The following items should be checked. Copies of items 1 and 2 should be obtained for the project files.

- 1. Pending compliance schedules,
- Construction and/or operating permits pertaining to source processes,
- 3. Past conditions of noncompliance,
- 4. Frequency of malfunctions reports, and
- 5. History of abnormal operations.

The inspector should also obtain a copy of appropriate plant layout drawings for use in preparing the audit inspection report. If possible, the files should be reviewed before entry to the plant so that important characteristics will be more easily remembered.

The inspector should prepare a concise file containing basic plant information, process descriptions, flowsheets, and acceptable operating conditions (Appendix A). It should contain the following to facilitate inspections and/or preparations:

 A chronology of control actions, inspections, and complaints concerning each major source in the plant;

- 2. A flowsheet identifying sources, control devices, monitors, and other information of interest;
- 3. The most recent permits for each major source, and
- 4. Previous inspection checklists.

Volume IV presents a recommended flow charting technique. In plants with complex control systems, it may be beneficial to review the technical literature and/or the complete agency file.

Based on reviews of agency and personnel files, the inspector should select a time when processes will probably be operating at representative conditions. The scheduling of time to visit plants with batch operations or other irregular operating schedules (e.g., seasonal) is especially important.

3.2 INSPECTION ANNOUNCEMENT

Written instructions from the Agency supervisory personnel should be obtained concerning the advance announcement of inspections. If it is desirable to announce the inspection in advance, leads of 1 day to 1 week are generally adequate to ensure that the necessary plant personnel will be available. The person contacted should have the authority to release data and samples and to arrange for access to specific processes.

3.3 INSPECTION EQUIPMENT

Necessary tools and safety gear should be carried in a portable case from source to source:

Carry at all Times

Hardhat
Safety glasses or goggles
Gloves
Coveralls
Safety shoes (steel tipped)
Ear protectors

Tape measure
Flashlight
Manometer or differential pressure gauges
Stopwatch
pH paper
Brass rods
Duct tape
Pry bar
Pocket guide of industrial hazards

Other equipment can be left in a central location until needed.

Carry When Needed

Pipe wrench Respirator with appropriate cartridge Velometer Pump and filter system Bucket Combustion gas analyzer Thermometers or thermocouples Multimeter Sample bottles Strobe Inductance ammeter . Tachometer Oxygen and combustibles meter Self-contained breathing equipment Pipe wrench Rope

Particularly important is the safety equipment--including the hard hat, the safety glasses, and the ear protectors. Remember, it is the inspector's responsibility to have safety equipment before entering the plant. Access to certain industrial facilities can be rightfully restricted or refused by plant representatives if designated equipment is not worn.

3.4 PLANT SURROUNDINGS

Observations of areas surrounding the plant may reveal a variety of signs of operational practices and pollutant emissions which can aid in the preentry evaluation, including:

- 1. Obvious vegetation damage near the plant,
- 2. Odors downwind of the plant,

- 3. Deposits on cars parked closeby,
- 4. Other signs of "dusting" downwind of the plant,
- 5. Fugitive emissions near plant boundaries,
- 6. Conditions around the product and/or waste storage piles, and
- 7. Conditions near lagoons and sludge ponds.

Some of the signs may mean that fugitive emission sources should be added to the inspection agenda. If odors are a problem, the weather conditions should be noted for later inclusion in the inspection report. Once inside the plant, olfactory fatigue may (under certain circumstances) reduce the inspector's ability to detect odors.

3.5 PLANT ENTRY

Upon arrival at the plant offices, the inspector should contact a responsible official to gain access to specific areas. If requested, the inspector should display an employee identification card which includes a photograph, and a physical description including, but not necessarily limited to, height, color of eyes, and color of hair. Visitor release forms generally can be signed as long as they in no way restrict the scope of the inspection.

If entry is refused for part or all of a facility within the scope of the inspection, obtain 1) reason(s) for refusal of entry, 2) plant official's name and title, and 3) time and date entry was requested. Notify supervisory personnel by telephone immediately. <u>Under no circumstances</u> should field inspectors attempt to summarize the potential legal consequences of refusal of entry.

3.6 PRE-INSPECTION INTERVIEW

The inspector should plan the initial interview with the plant manager or other responsible officials prior to the inplant inspection. Some of the points for discussion are:

- 1. The purpose of the inspection,
- 2. The type of measurements to be made,
- 3. The samples (if any) to be acquired,
- 4. The systems to be evaluated,
- 5. Changes in plant management that need to be noted in the main file,
- 6. Process flowsheets needed to confirm that operational conditions in the file still pertain, and
- 7. Operating records required by Standards of Performance for New Sources (NSPS) and/or for determinations of operating conditions specified in permits.

Applicable regulatory requirements should be reviewed carefully, and their apecific applications to the source in question should be discussed with appropriate engineering and/or legal staff.

Other issues the inspector should be prepared to discuss include:

- 1. Authority for the inspection,
- 2. Agency organization,
- 3. Scope, timing, and organization of the inspection (preferred inspection agenda), and
- 4. Treatment of confidential data.

The inspector should ask plant officials about the operational status of all processes and pollution control equipment within the scope of the inspection and about the types and frequencies of any malfunctions. If equipment is not at or near normal conditions, the reasons for deviation should be noted, and the times when units can be expected to achieve representative operations should be recorded for use in scheduling follow-up inspections, if necessary.

SECTION 4

COUNTERFLOW INSPECTION

The inspector starts the inspection at the gas exhaust point (or endpoint) of the process and proceeds through the process flow to the point where raw materials are input. Each step shown on the flowsheet of Figure 1 should be based on data from previous steps to derive increasingly precise analyses. Examples of data received at each step are listed in column 2 of Table 1; the evaluations in column 3 gradually focus on air pollution control effectiveness as the inspection continues, due to the expanding data base in column 4. By the time the in-plant inspection has ended, a series of ten or fifteen distinct observations should provide a consistent and logical assessment of performance conditions.

4.1 STEP 1: OBSERVE THE STACK EFFLUENT

The opacity readings^a of emission points should be observed using Method 9 procedures. PEDCo recognizes that an agency can, in many cases, develop a legally and technically sound case solely on the basis of visible emission observations. In some cases, however, it is possible that the value of opacity information will be primarily for diagnosing changes in system performance. The following paragraphs describe how the Counterflow Technique includes this diagnostic requirement.

^aOnly staff with currently valid Visible Emission Certificates should make these observations. It should be recognized that an agency may choose to initiate enforcement actions directly on the basis of these observations.

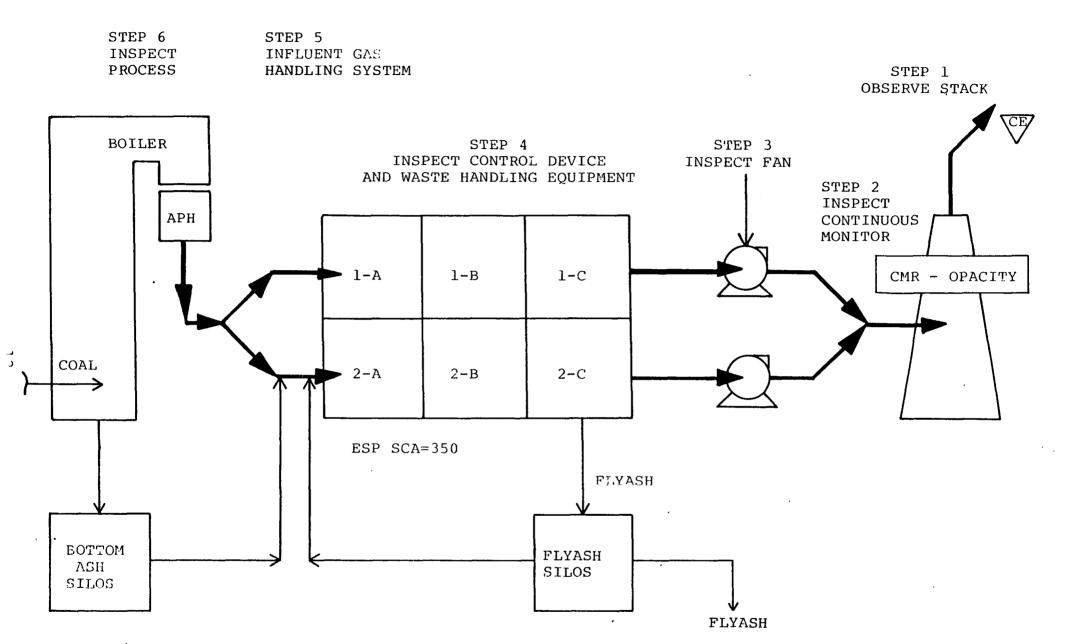


Figure 1. Steps in Counterflow Inspection Technique for coal-fired utility boilers controlled by a "cold side" electrostatic precipitator.

TABLE 1. COUNTERFLOW TECHNIQUE, UTILIZATION OF DATA

Step	Data obtained	Preliminary evaluation	Support data and steps obtained
1. Stack effluent	Change in opacity reading Presence of detached plume Presence and timing of puffs Colors of emissions	None	None
2. Continuous monitors	Change in opacity reading SO ₂ and NO _x concentrations Temperature of gas stream	Have emissions increased to the point of possible noncompliance?	Opacity - step 1
	Intermittent emission spikes Representativeness of inspec-	Has size distribution of particles changed?	Opacity - step 1 Color - step 1
	tion period (review of records)	Are there intermittent emission problems?	Puffs - step 1
3. Induced draft fan	Fan static pressure	Has system pressure drop changed?	None
	Fan R.P.M.	Has control system been bypassed?	
	Fan motor current	Is effluent diluted?	
	Gas temperature	Has gas flow rate changed?	
	Fan wheel vibration	Is demister operating satisfactorily?	
	Fan housing condition	Has operation changed fan R.P.M.?	
	Fan damper position		
Inspection stop point		Is further inspection necessary?	Opacity - step 1 Opacity - step 2 Gas temp - step 2 or 3 Fan static pressure - step 3 Fan motor current - step 3 Fan R.P.M step 3
4. Air pollution control device external inspection	Static pressure drop Cleaning system operation Hopper condition	Has gas flow rate increased or decreased substantially?	Opacity - steps 1 and 2 Gas temperature - step 2 or 3 System pressure drop - step 3 Fan motor current - step 3
	Liquid flow rate Liquid temperature	Has mass loading increased?	Opacity - steps 1 and 2 System pressure drop - step 3
	Liquid pH Electrical parameters	Has particle size distribution changed?	Opacity - steps 1 and 2 Color of plume - step 1
	Rapper operation Solids/liquids discharge rate	Are operating and maintenance practices adequate?	

(continued)

TABLE 1. (continued)

Step	Data obtained	Preliminary evaluation	Support data and steps obtained
Inspection stop point		Is further inspection necessary?	Results of previous analyses, plus comparison of control device actual and baseline parameters (diagnostic score)
5. Ventilation system ductwork (effluent delivery)	Hood capture velocities Static pressures along ductwork Gas temperatures	Have gas flow rates changed?	Fan current - step 3 Fan static pressure - step 3 Control equipment static pressure drop - step 4
:	Condition of cleanout traps	Are gas streams being diluted?	Gas temp - steps 2 and 3
	Integrity of ductwork	Are all sources being operated?	
6. Process equipment	Production data Process monitors Raw material information and samples	Has production rate increased?	Gas flow rate - step 5 Static pressure data - steps 4 and 5 Solids discharge rates - step 4 Opacity - steps 1 and 2 Fan motor current - step 3 Fan static pressures - step 3
		Have operating conditions changed?	•
		Have raw material characteristics changed?	
,		Has particle size distribution of effluent changed?	Opacity - steps 1 and 2
•		Can an internal inspection of control equipment be conducted safely?	
Inspection stop point		Is an internal inspection of air pollution control devices necessary and feasible?	Process operating conditions - step 2 Control device conditions - step 4
7. Air pollution control	Clean side deposits		
device (external inspection)	Alignment of electrodes - ESP		
mspeccion	Insulator conditions		
	Fabric condition	•	
	Gas distribution plate/vane conditions		
	Air inleakage through welds and holes		Confirm preliminary evaluations - steps 1 through 6
	Hopper conditions		

In most cases, there is a relationship between the opacity observed during the inspection and the mass emissions penetrating the control device. Regardless of the mathematical form of this relationship, as the opacity increases, the mass emissions generally increase. In Figure 2a, Case 1 represents the most sensitive relationship—a small increase in opacity indicates a large increase in mass emissions; however, errors inherent in a small opacity increase can make any conclusions meaningless in this case. Case 2 presents "contrary" problems—above a certain upper opacity level, there is no change in mass emission rates; thus, at this level, opacity has no diagnostic value. The ideal case is the linear relationship of Case 3; fortuitously, this is generally the prevailing relationship in most industries.

Despite the best efforts of regulatory development personnel, the mass emission regulations and opacity regulations may not always agree. Linear relationships illustrate these possible disagreements in Figure 2b. Case 4 represents the intended situation; that is, any violation of an opacity regulation also involves a violation of the mass emission regulation. In Case 5 there is a substantial opacity violation without a violation of the mass standard. In other cases (represented by line segment 6), a violation of mass emission standards might not be suspected due to decreased sensitivity to opacity. The point is: in certain cases the absolute magnitude of the observed opacity is most useful when the opacity-mass relationship is known.

In the diagnostic phase of the Counterflow approach, the procedure uses (whenever possible) a change in opacity (observed versus historical) rather than an absolute magnitude of observed opacity. Regardless of the opacity-mass relationship, (or the mathematical form) a change in opacity does indicate a change in mass emissions. This information supported by a set of facts herein provides the conclusions sought in a plant inspection using the counterflow procedure.

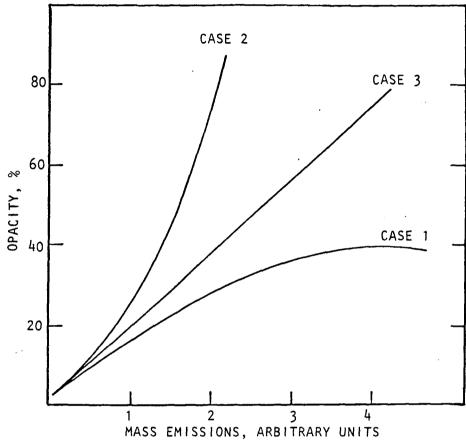


Figure 2a. Opacity-mass relationships.

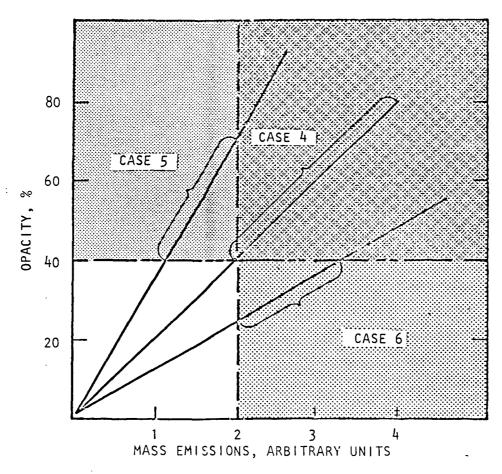


Figure 2b. Opacity and mass emission violations.

The color of the effluent is another plume characteristic which should be observed. For fossil fuel combustion sources, the color is an indirect indication of operating conditions. The following list (Table 2) was compiled by EPA's Control Programs Development Divisions:

TABLE 2. PLUME CHARACTERISTICS AND COMBUSTION PARAMETERS

Plume color	Possible operating parameters to investigate
White	Excess combustion air; loss of burner flame in oil-fired furnace
Gray	Inadequate air supply or distribution
Black	Lack of air; clogged or dirty burners or insufficient atomizing pressure, improper oil preheat; improper size of coal
Reddish brown	Excess furnace temperatures or excess air; burner configuration
Bluish white	High sulfur content in fuel

For other types of sources, the color may not be as variable or may not have a distinct meaning with respect to the process or the control equipment. Nevertheless, a <u>change</u> in the color indicates a change in the system. For example:

- 1. Increased quantities of bluish particulates generally indicate increased generation of very small particles (0.1 to 2 microns) which are difficult to collect in most control devices.
- 2. A detached plume indicates fairly conclusively that particulates are forming as the vapors are released to the cold ambient air; detached plumes often cause serious corrosion problems, since any cold surface in the system is susceptible to acid-mist condensation.
- 3. The frequency and duration of "puffs" from the stack are often caused by rapping reentrainment problems in electrostatic precipitators (ESP's) or by fabric leaking/cleaning problems in baghouses. Cyclic process conditions can also lead to puffs.

4.2 STEP 2: CHECK THE CONTINUOUS MONITORS

After observation of the stack effluent, the next logical step is to check the continuous monitors downstream from the control equipment.

- 1. The operation of the purge air blowers should be confirmed and the alignment of the source and retroreflection should be checked.
- 2. The actual path length should be compared with the value used in the instrument calibration.
- 3. In almost all cases, the zero and full-scale settings can be checked and confirmed without taking the instrument offline.
- 4. The status of the window inductor light should be checked.
- 5. Also, the appearance of the instrument recording trace and the changes in recorded values may indicate reliability or unreliability of continuous monitor data.

Process operating personnel should be able to supply data on the technique and the frequency of calibrations.

The continuous opacity monitor (commonly called a transmissometer) indicates intermittent emission spikes caused by
rapping reentrainment (ESP's); pulse flexing of bag seams
(fabric filters); and other problems. A brief scan of the last
24 hours of chart paper may help to identify these problems and
to describe system performance.

The transmissometer data should be used to confirm and clarify the opacity observations in step 1. Instrument problems should be suspected when there are substantial differences between the opacity recorded in step 1 and that indicated on the monitor. If the instrument response time and the recorder chart speed have been set properly, it will be possible to check for trends in the opacity levels.

1. A cyclic pattern suggests variation in process operating conditions; and

2. A continually deteriorating pattern suggests a developing control device problem which is likely to demand the attentions of the operator and the inspector; the deterioration can also suggest a gradual drift of the instrument or accumulation of dirt on the optical surfaces.

Failure to properly operate and/or maintain an opacity monitor can constitute a violation of regulations.

In step 2, the inspector should have:

- 1. Confirmed the visible emissions status with respect to opacity regulations,
- 2. Confirmed the installation and operating status with respect to continuous monitor regulations, and
- 3. Developed a preliminary idea of the process and the control device operating conditions.

As yet, there would not be enough information to evaluate mass emissions in cases where a reliable opacity-mass emission correlation has not been identified.

4.3 STEP 3: MEASURE THE FAN OPERATING PARAMETERS

Three operating parameters of the induced draft fan are useful in interpreting control system operations:

- 1. Increase in total static pressure across the fan,
- 2. Electrical current drawn by the fan motor, and
- 3. Revolutions per minute (R.P.M.'s) of the fan wheel.

Evaluated together these parameters indicate the gas flow rate and the total system pressure drop. These changes are important in diagnosing control system operating conditions.

If the fan parameters are not monitored at the plant, the inspector should use an inductance ammeter, a manometer (or magnehelic gauge), and a tachometer (or a strobe in cases where the tachometer cannot be used). The inspector should request that static pressure taps be made in the ductwork leading to and from the induced draft fan. The inspector should not drill or cut these holes unless the plant manager approves. Once

taps are available, the static pressures at the fan inlet and outlet should be measured using the set of magnehelic gauges.

The fan data can be used to <u>estimate</u> the gas flow at the time of the inspection. After correction of all readings to standard conditions, refer to the appropriate set of characteristic curves to determine SCFM. Please remember that this is only an estimate and is subject to errors due to variability in fan performance, site-specific gas flow factors, and physical condition of the wheel. The remainder of this section concerns means to utilize fan data to <u>diagnose changes</u> since the previous Counterflow Inspection. (Note: in most cases the baseline data will not be available since fan parameters are not measured in conventional inspections).

The type of fan used by most industrial sources with particulate-laden effluents is the radial blade centrifugal Its operating parameters are illustrated in Figure 3; this curve applies to a New York Blower Company size 332 general induced draft fan with an LS wheel operating at 1460 R.P.M.'s at standard conditions. As indicated, the static pressure losses in the control equipment and ductwork (curve A) increase proportionally with the square of the flow rate. fan, however, develops less static pressure at higher flow rates, and thus it has a strong negative slope (curve B). The intersection of the system line and the fan pressure drop curves define the operating point of the system. point, the gas flow rate is 8,400 SCFM, and the brake horsepower (curve C) is approximately 24.5. Figure 3 should be used as baseline data in considering:

- 1. The potential effects of gas temperature,
- 2. The changes in system static pressure drop, and
- 3. The changes in fan speed.

Changes in the rotation speed of the fan wheel is possible in many belt-driven units as shown by the curves in Figure 4. In Case 1, an R.P.M. increase leads to a greater gas flow rate and

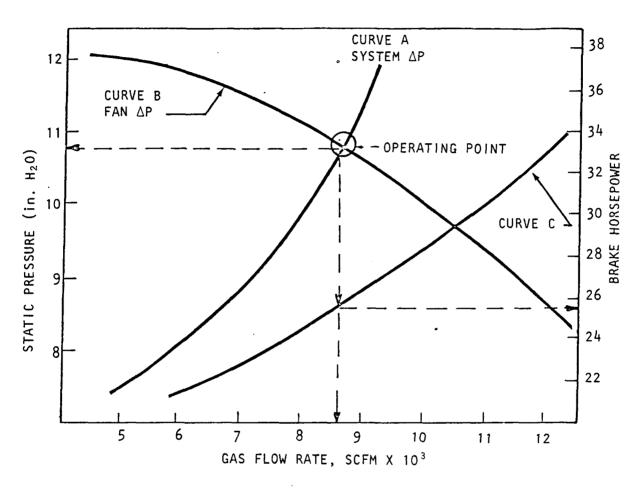


Figure 3. Operating characteristics of radial blade centrifugal fan (New York blower size 332 with LS wheel @ 1460

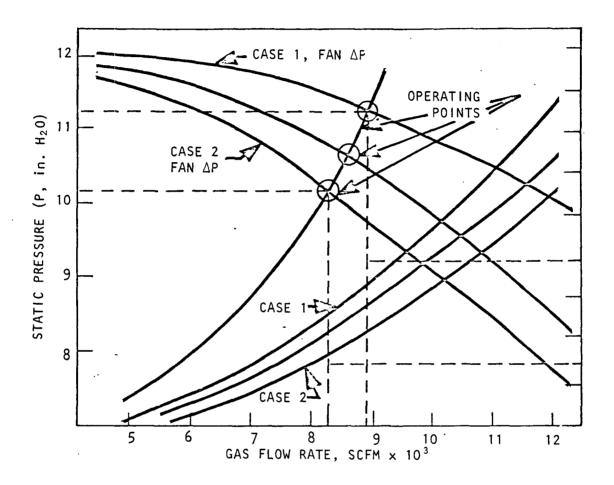


Figure 4. Fan characteristic curves, effect of R.P.M. change.

higher static pressure. Increasing the R.P.M. is the course of action at plants where process gas flow is insufficient; however, this can dangerously increase tip speed, and it can adversely affect fabric filters or ESP's. The opposite situation is illustrated in Case 2. An R.P.M. decrease (perhaps to save energy cost) can decrease the flow substantially; this can reduce the collection efficiency of cyclones and wet scrubbers since these depend on impaction for particle collection and since impaction efficiency is directly dependent on gas velocity. Increases in the fan wheel R.P.M. can occur because of intentional actions of the operator. (Belt shippage can reduce R.P.M. without operator's knowledge).

Other changes in fan operation can occur with or without the operator's knowledge. For example, the fan motor current decreases when the static pressure drop increases; Case 3 in Figure 5 represents total system pressure drop increases. Accompanying this Case 3 change should be an increase in the fan motor current as indicated in Figure 5. As indicated in Table 3, this change can be due to a variety of process and control device operating factors. Pressure drop decreases can be caused by (partial list):

- Decreased effluent gas flow rate, and/or
- Operating conditions such as control device shortcircuiting (open access doors, gaps in ductwork, open by-pass dampers), and
- 3. Decreased scrubber liquor flow.

The cause of the change can be further analyzed by considering the measured gas temperature at the fan inlet. A low temperature suggests either an open access hatch or a serious leak in the ductwork.

System diagnoses are based on <u>changes</u> in the three fan operating parameters. All three (total static pressure, motor current, and wheel R.P.M.) must be measured since all three are analyzed as a set. (The Counterflow Procedure does <u>not</u> require

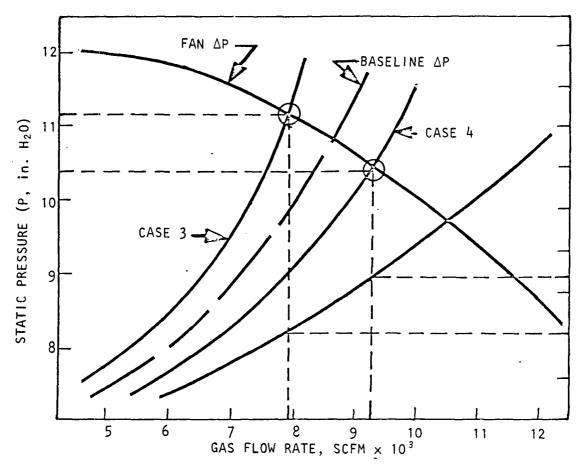


Figure 5. Fan characteristic curves--effect of system pressure drop change.

knowledge of fan characteristic curves.) With these, the inspector should be able to determine if abnormal conditions exist and which of the four cases is applicable.

In addition to analyzing the operation of the fan, the inspector should observe the physical condition of the fan. If it is possible to physically inspect the fan (be sure it is locked off), note the presence of:

- 1. Blade abrasion,
- 2. Deposit buildups, and
- 3. Corrosion of the wheel and fan housing.

The first two problems indicate excess emissions of large particles (10μ) and demister malfunction. The third problem could be due to both the overloading of the demister and excess emissions of corrosive gases. The induced draft fan operating parameters indicate a number of important changes in control device operating conditions (Table 3). The measured parameters were corrected for the gas temperature at the fan inlet by using the factors in Table 4.

At the end of step 3, the inspector should decide whether or not further on-site efforts are necessary to determine compliance with mass emission standards. If the fan operating parameters (static pressure, motor current, and R.P.M.'s) are $\pm 10\%$ and if the gas temperature at the fan inlet is $\pm 20^{\circ}$ F, it is unlikely that mass emissions have changed significantly. In some cases, the field inspection can be terminated with step 3. Generally, it is necessary to inspect the control equipment (step 4) to confirm the evaluations of steps 1, 2, and 3.

4.4 STEP 4: ANALYZE CONTROL DEVICE PERFORMANCE

Based on the previous three steps in the Counterflow Procedure, the inspector should have a preliminary estimate of the following:

1. Present gas flow rate through the control system and changes since last Counterflow Inspection,

TABLE 3. INTERPRETATION OF FAN OPERATING CONDITIONS (RADIAL BLADE TYPE ONLY)

•		Fan paramet		
Case	Calculated ∆P _{sp} at 70°F	Calculated Amps at 70°F	Fan wheel R.P.M.	Possible causes
1	Decreased	Decreased	Decreased	Operator decreased R.P.M.
2	Increased	Increased	Increased	Operator increased R.P.M.
3	Increased	Decreased	Unchanged	 a) Filter blinding b) Filter cleaning problem c) Hopper overflow d) Scrubber bed pluggage e) Decreased gas flow f) Damper partially closed
4	Decreased Increased		Unchanged	a) Baghouse leaks b) Shortcircuiting c) Decrease in liquor flow d) Increase in gas flow e) Damper partially open

TABLE 4. FAN DATA, TEMPERATURE CORRECTION^a

Temp F	Factor	Temp F	Factor
20	0.91	320	1.47
40	0.94	340	1.51
60	0.98	360	1.55
80	1.92	380	1.59
100	1.06	400	1.62
120 140 160 180 200	1.09 1.13 1.17 1.21 1.25	420 440 460 480 500	1.66 1.70 1.74 1.77
220	1.28	520	1.85
240	1.32	540	1.89
260	1.36	560	1.92
280	1.40	580	1.96
300	1.43	600	2.00

^aAdapted from "Basic Energy/Environment Analysis", NAPA information series 67, by C. Heath, August 1978.

- 2. Present total system static pressure drop and changes since last Counterflow Inspection,
- 3. <u>Changes</u> in particulate emission levels since last stack test or Counterflow Inspection,
- 4. Present temperature of the effluent, and
- 5. Presence of cyclic or intermittent emissions.

Results of these five observations should provoke specific questions to guide the inspection of the control system.

When inspecting the control device and its auxiliary equipment, the inspector should proceed in a logical sequence to obtain the information needed for evaluating the performance. Detailed checklists (Appendix B) have been prepared for wet scrubbers, fabric filters, and ESP's. The general approach to all three is to use checklists as the inspector proceeds from the control room (if applicable) to the control device. These checklists are arranged to facilitate the inspection. The checklists include preliminary diagnostic sections (Tables 5-7) which are arranged according to commonly encountered problems.

For example, the ESP diagnostic sheet includes, but is not limited to:

- 1. Particle resistivity changes,
- Insulator failures,
- 3. Broken discharge wires, and
- 4. Nonuniform gas distributions.

Under the each problem category is a list of readily observed symptoms and the relative importance of each as indicated by a rating factor. If the sum of the factors under any category is >10, there is a reasonable probability that a problem does exist; if so, further inspection and/or testing is needed and should be recommended in the inspection report.

In most plants, it will be impractical to observe every item listed in Figures 6-8 or to observe every symptom listed

TABLE 5. FABRIC FILTERS COUNTERFLOW INSPECTION DIAGNOSTIC SECTION

Poss	ible Operating Problems	Average Baseline (Specify Value)	Observed (Specify Value	Location*	Abnormal (Check)	Rating (1-10)	Recommended Action
Á,	Bag Tears or Pinholes			•			
	1. Filter house pressure drop low (<80% avg.) 2. Opacity high 3. Bag age high (typical av 4. Some bags inaccessible 5. Design A/C high (>120% a 6. Actual A/C high (>120% a 7. Wear plate eroded 8. Frequent high excursions	vg.)	N/A N/A	E E I E E I		3 5 5 2 4 4 3 4	If sum (I) of ratings is > 10 perform internal inspection. Check for deposits on filter house clean side. Check inaccessible bags. Use fluorescent dye technique. Check integrity of fabric by attempting to extend rips.
В.	Bag Blinding				-,	· -	
	 Filter house pressure drop high (>150% avg.) 			E		7	If sum (Σ) of ratings is ≥ 10 , perform internal inspection.
	 Opacity low Cleaning frequency high (cycles/day) 			e E		2 5	Check dirty side of bags for coatings (this may be difficult to identify in some
	4. Gas temp low (<20°F avg. 5. Hoisture in gas stream	N/A	N/A	E E		4	cases). Check records for steady rise in filter house
	6. Particulate sticky 7. Air in-leakage (hoppers/access doors)	N/A	N/A N/A	E		4 2	pressure drop. Reschedule inspection in near future.
	8. Unit not insulated	N/A	N/A	E	***************************************	2	
c.	Bag Bleeding				 	<u> </u>	
	1. Opacity high 2. Pressure drop gradually			e E		5 2	If sum (Σ) of ratings is ≥ 10 , attempt to confirm uses of
	increasing 3. Cleaning frequency high			E			fluorescent dye and black light.

^{*}Location: E is external, and I is internal.

TABLE 5 (Continued)

Ровв	ible Operating Problems	verage Baseline (Specify Value)	Observed (Specify Value	Location*	Abnormal (Check)	Rating (1-10)	Recommended Action	
D:	Cleaning System		,					
•	1. Filter house pressure dra high 2. Pulse-jet air header pres sure low 3. Solenoids inoperative 4. Reverse air fan inoperative 5. Shaker motor inoperative 6. Bag length long 7. Equipment inaccessible 8. High intensity cleaning required	N/A	N/A N/A N/A	E E or I T or I E or I E I E		5 5 10 10 2 2 2	If sum (Σ) of ratings is >10, perform internal inspection and check deposits on dirty vide of bags. Check bag tension. Reschedule inspection in near future.	
E.	required Σ = Hopper							
	 Filter house pressure drop high Solids-removal run intermittent Indicator level existent and/or inoperative 		N/A N/A	E E		5 3 2 2	If sum (Σ) of ratings is >10, perform internal inspection of hoppers.	
·	4. Heaters nonexistent and/inoperative 5. Vibrators nonexistent and/or inoperative 6. Hopper valves corroded 7. Hopper slope <60° 8. Hoppers not insulated 9. Winter 10. Hammer markings on hoppe	N/A N/A N/A N/A	N/A N/A N/A N/A N/A N/A	E P. 1 E E E E		2 3 2 2 2 2		
	walls 11. Conveyor inoperative	N/A	N/A	E		ε - 10		

^{*}Location: E is external, and I is internal.

TABLE 6. SCRUBBERS COUNTERFLOW INSPECTION DIAGNOSTIC SECTION

Possil	_	age Baseline ecify Value)	Observed (Specify Value		Abnormal (Check)	-	Recommended Action
۸. ١	No Liquor Flow		,				•
	Pumps are inoperative Inlet and outlet gas temps same	N/A N/A	Yes, No N/A	E E		10 10	If sum (E) of ratings >10, request immediate correction action, and/or stack test.
:	3. Opacity high			E		5	
	4. Scrubber pressure drop low			E		5	
	5. Nozzles plugged	N/A	Yes, No	I	 ,	7	
B. 1	Low Liquor Flow					4	
1	l. Nozzle operating pressure (<80% avg.)			E	•	3	If sum (E) of ratings is >10, attempt to measure exit water
:	2. Gas temp high (10% above avg.)			E		3	flow rate to confirm conclusions. Request stack test.
	3. Opacity high			E		5	•
•	4. Recirculation liquor pH low (<5)	,		E		3	
	Flow rate monitor value low (<80% avg.)			E		7	
	6. Scrubber pressure drop low (<80% avg.)			E		3	•
	 Exit water temp high (>20% above avg.) 	***************************************	· 	E		Σ =	
C. Gi	Gas Flow Rate High						
	l. Opncity high			E		5	If sum (E) of ratings is ≥ 1
	2. Outlet gas stream temp			E		5	check process equipment and
	high (>20°F above avg.)			·E		5	production rate.
	Exit water temp high			E.			

*Location: E is external, and I is internal. (Continued)

TABLE 6 (Continued)

Possi	bla Operating Problems	Average Baseline (Specify Value)	Observed (Specify Valu	Location* e)	Abnormal (Check)	Rating (1-10)	Recommended Action
D.	Gas Flow Rate High						
	 Opacity high Temp of outlet gas low (>20°F below avg.) 	**************************************	*************	E E	-	5 5	If sum (E) of ratings is >10, check process equipment and production rate. Request stack
	3. Temp of exit liquor low (>20°F below avg.)			E	,	5	test if problem is serious.
	4. Scrubber pressure drop 1 (<80% avg.)	.ov		E			
E.	Bed Plugging						
	1. Scrubber pressure drop h (>40% above avg.)	iigh		E	. ——	5	If sum (E) of ratings is >10, check for bypassing of effluen
	2. Liquor turbidity high 3. Liquor pH high (>8)	N/A	N/A	e E		5 5	around scrubber. Request immediate corrective action.
F.	Nozzle Erosion				<u></u>	<u></u>	
	1. Nozzle operating pressur drop low (<80% avg.)	re		E		5	If sum (Σ) of ratings is ≥ 10 , recommend nozzle replacement.
	 Opacity high Liquor turbidity high 	N/A	N/A	E E		3 3.	·
	4. Corrosive liquor 5. Nozzles unchanged in 6 months	N/A N/A	N/A N/A	. E		3	•
	6. Nozzles operable	N/A	N/A	I		10 r =	

*Location: E is external, and I is internal. (Continued)

TABLE 6 (Continued)

Post	sible Operating Problems	Average Baseline (Specify Value)	Observed L (Specify Value)	ocation#	Abnormal (Check)	Rating (1-10)	Recommended Action
G.	Demister						
	 No water flow to demis Gas velocity high (>10 per second) Fan vibrating 			I E E		5 10 5	If sum (Σ) of ratings is \geq 10, check for changes in production rate. Reschedule inspection in near future in anticipation of fan unbalance problem.
н.	Venturi Throat Adjustment	·		 			
	 Scrubber pressure drop (<80% avg.) Visible evidence of ch Opacity high 		N/A	E E B		4 4 4	If sum (E) of ratings is >10, request corrective action immediately or request stack test.
ī.	Impingement Plate or Tray	Collapse		***************************************		·	
	 Pressure drop low (<80 Opacity high Build-up of liquor in 		N/A	E E I		ξ =-	If sum (I) of ratings is >10, attempt internal inspection.
J.	In-lcakage of Air 1. Temp of gas stream low 2. Obvious shell corrosion		N/A	e I		5 5 Σ -	If sum (Σ) of ratings is >10, attempt internal inspection.

^{*}Location: E is external, and I is internal.

TABLE 7. ELECTROSTATIC PRECIPITATORS COUNTERFLOW INSPECTION DIAGNOSTIC SECTION

ossible	Operating Problems	Average Baseline (Specify Value)	Observed (Specify Value	Location*	Abnormal (Check)	Aating (1-10)	Recommended Action
. ELE	CTRICAL Particle Resistivity						•
A				_		_	70 40 4 10
	1. Peak voltage low (down 5-10 kv)		 .	E		. 5	If sum (Σ) of ratings is ≥ 10 , request in-situ resistivity to
	2. Rapping intensity			E		.5	and check sulfur content of
	increased						fuel, moisture content of gas,
	3. Temp changed (+50°F			. E		3	and temperature of gas.
	4. Spark rate increase (±50 sparks/min)	a		£		,	
	5. Opacity high			e E		6	
	 Coal sulfur content low (<1.0%) 			E		Ε - 6	
В.	Transformer-Rectifier	Set Problems					
	1. No secondary curren	t N/A	N/A	E		10	If sum (Σ) of ratings is ≥ 10 ,
	2. No penthouse purge	N/A	N/A	E E		2	request repair.
	3. Voltage zero, curre	nt N/A	N/A	E		10	
	high 4. Opacity high			E		6 _	
						Σ -	
c.	Insulator Failure						
	1. Peak voltage low			E		5	If sum (E) of ratings is ≥ 10 ,
	2. Penthouse purge (no used)	N/A	N/A	E		. 5	request repair.
	3. Penthouse temp high	1		E		3	
	(+20°F)			ç		6	
	4. Opacity high 5. Cracks visible	N/A	-N/A	E I		10	

⁽Continued)
*Location: E is external, and I is internal.

TABLE 7 (Continued)

Possible	Operating Pro		rage Baseline pecify Value)	Observed (Specify Value)	Location*	Abnormal (Check)	Rating (1-10)	Recommended Action
D.	Broken Disch	arge Wiren						·
	 Deposits Violent m tuating 		N/A N/A	N/A N/A	R I		5 10	If sum (Σ) of ratings is ≥ 10 , request repair.
		vel indicator	А\и	N/A	E		2	
	4. Spark rat sparks/mi			· ·	E		5	
	5. Opacity h 6. Broken di	igh scharge wires	N/A	N/A	E		3 10	
II. GAS	FLOW Excessive Ve	locity						
	1. Flow rate 2. Voltages rents lov	high, cur-			E		5 5 ·	If sum (E) of ratings is >10, check production and/or genera-
	3. Opacity 1				E		Σ = 5	
в.	Nonuniform I	Distribution					•	
	1. Flow rate 2. Secondary nonparall	currents	N/A	N/A	e E	<u> </u>	2 5	If sum (I) of ratings is ≥ 10 , request velocity traverse.
	3. Hopper 1	evels differ- parallel			1		5	•
	4. Rappers	on distribu- tes not used	<u> </u>	N/A	E or I		Σ = .	

*Location: E is external, and I is internal.

(Continued)

TABLE 7 (Continued)

Possi	lble	. •	erage Baselina Specify Value)	Observed (Specify Value		Abnormal (Check)	_	Recommended Action			
III.	НЕСН А.	LANICAL Rapper Problems									
		1. Puffs visible 2. Peak voltage changed, secondary current	N/A	N/A_	e E		5	If sum (E) of ratings is >10, request internal inspection by plant personnel. Request inter			
		constant 3. Spark rate changed 4. Low sulfur coal used 5. Dust sticky	N/A	N/A	E E		3 3 3	sity measurement, if approp			
	В.	Hopper Solids Removals									
		Broken discharge wire Mass loading probably increased		N/A N/A	I E		5 5	If sum (Σ) of ratings is \geq 10, request internal inspection and/or changes in operational			
		3. Nonuniform gas distri	- N/A	N/A	E	-	3	practices.			
		4. Hoppers not emptied	N/A	N/A	E		5	•			
		continuously 5. Level indicators not used	N/A	N/A	E		3				
·		6. Heaters not used 7. Vibrators not used 8. Hoppers not insulated 9. Corrosion around out-		N/A N/A N/A N/A	E E E I		2 2 2 3				
		let valves 10. Hopper slope <60° 11. Hoppers full or bridged	N/A N/A	N/A N/A	E		E - 10				

*Location: E is external, and 1 is internal.

(Continued)

TABLE 7 (Continued)

Possible	•	erage Baseline (Specify Value)	Observed (Specify Value	Location*	Abnormal (Check)	Rating (1-10)	Recommended Action
III. MEC C.	CHANICAL (continued) Collection Plate Warp are	nd Malelignment					
	 Change in air load Repeated hopper over- flow 	N/A N/A	N/A N/A	E or I		5 3	If sum (Σ) of ratings is \geq 10, request alignment check.
	 Air in-leakage Malalignment visible 	N/A N/A	N/A N/A	e I		3 10	
IV. EFF	PLUENT CHARACTERISTICS Mass Loading Increases						
	1. Opacity high	•				6	If sum (E) of ratings is ≥ 10 ,
	2. Inlet section, secondary currents low			12		. 5	check production and/or genera- tor rate.
	3. Hopper unloading frequency increases	• · · · ·		E		<u> </u>	

^{*}Location: B is external, and I is internal.

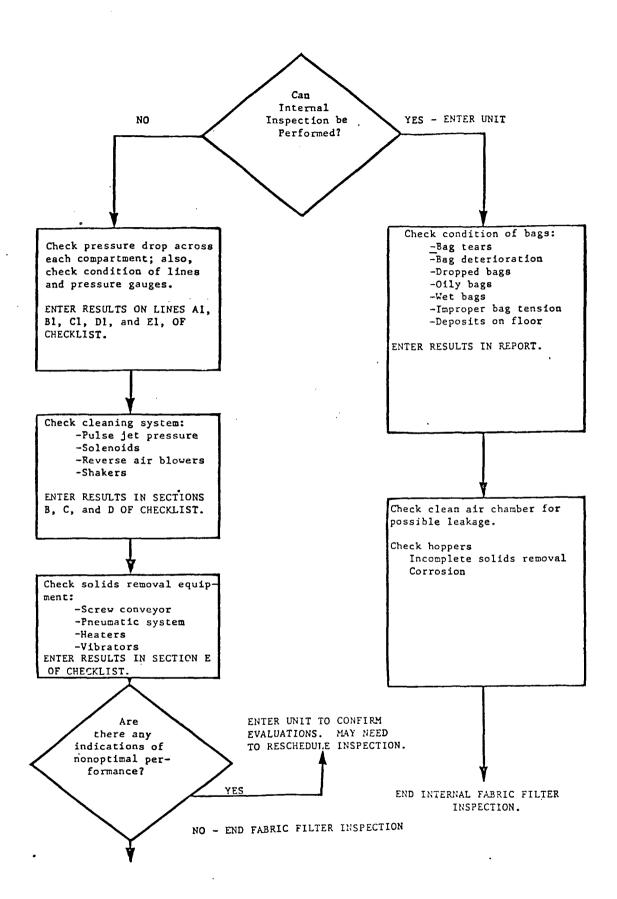


Figure 6. Fabric filter inspection flowsheet.

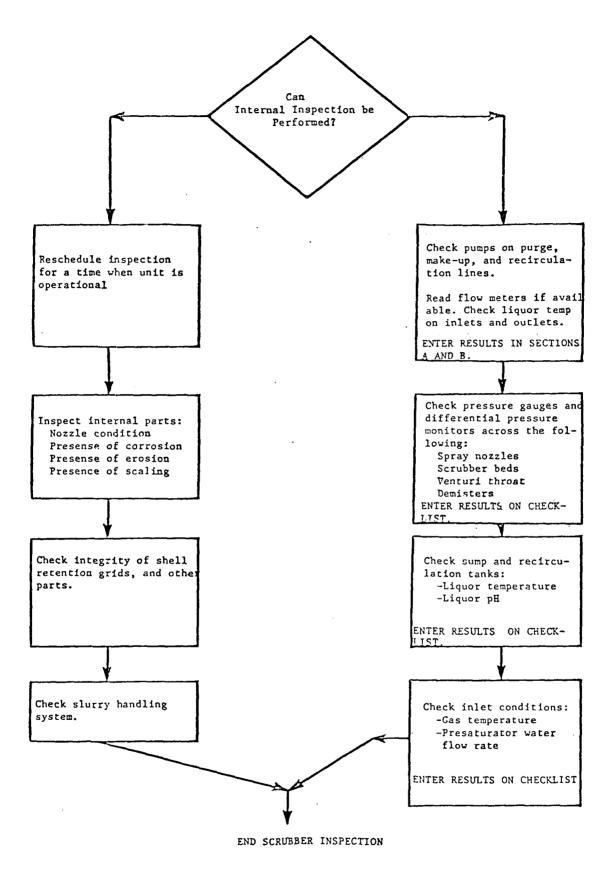


Figure 7. Scrubber inspection flowsheet.

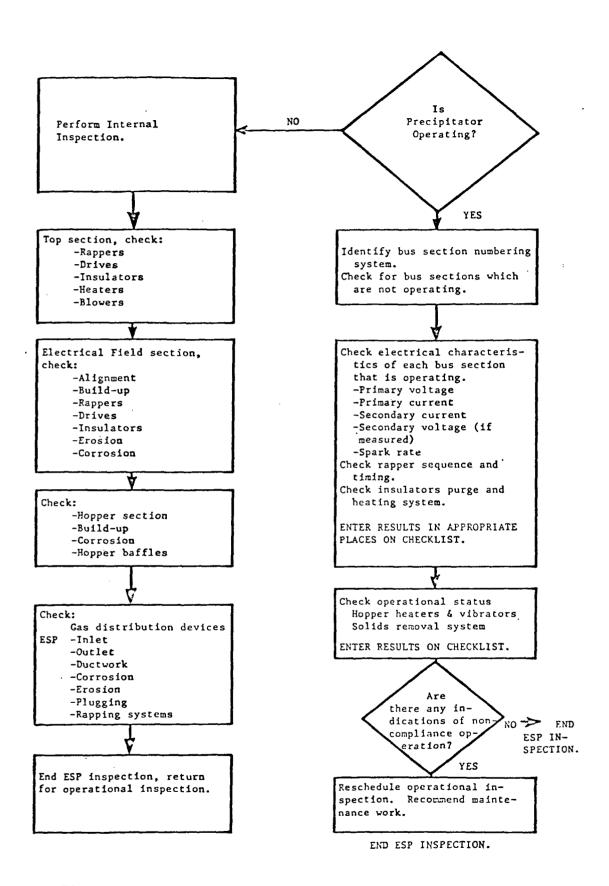


Figure 8. Electrostatic precipitator inspection flowsheet.

in Tables 5-7. This is why the diagnostic sheets are designed to reflect combinations of observations. In the extreme situation where there are essentially no equipment monitors and where access to components is restricted, the difficulty and limitations involved in performance evaluation should be noted in the inspection report.

During each stage of the control device evaluation, the inspector should compare the observed operating conditions with the baseline values obtained from compliance stack tests or from manufacturer's specifications. Deviations from site specific baseline values are the best indicators of abnormal performances.

The following discussions of control devices do not extend to standard design methodology and operating procedures. It is assumed that the field inspector is familiar with most control devices and has performed in-plant inspections in the past.

4.4.1 Fabric Filters

Five major categories of fabric filter operating problems are listed in the left column of Table 5. Only one of these-Bag Tears/Pinholes--causes immediate excess emissions. The others strain the fabric to the point that extensive repair and/or replacement is eventually necessary.

There are two basic approaches to the inspection of fabric filters. With the most common one, the unit is not shutdown during the inspection. The field inspector should decide if the observed performance symptoms call for a follow-up internal inspection and if a stack test should be recommended. With the second approach, the system can be shutdown (or compartments isolated one-by-one) long enough to perform the internal inspection. If the opacity observed in step 1 and/or step 2 is high and if the internals are accessible, we highly recommend proceeding along the right-hand path of Figure 6. Internal checks are the only truely reliable means for identifying fabric filter problems. Only if access to the unit is impossible

do we suggest the use of the indirect approach illustrated on the left of Figure 6; in this case, the inspector evaluates whether a return trip (when the unit is down) is justified.

Some of the symptoms on the diagnostic checklists are design factors. Fabric filter design is very significant with respect to long-term performance. Design deficiencies at any source should be checked routinely during each inspection.

4.4.2 Wet Scrubbers

To evaluate the performance of a wet scrubber, the PEDCo inspector should first confirm that the recirculation pump is operating. If there is no water/liquid circulating through the system, the inspector should recommend a follow-up inspection when the scrubber will be operational. If there is circulation, the inspector should proceed along the flow of water through the system (water flow is generally counter to gas flow).

Next, the inspector should confirm that the pumps are on, and if so, should read the flow meter (if any). In the line going to the spray nozzles, low pressure indicates erosion of the nozzles and likely increases in the water spray droplet size. If the line pressure does not change when the flow is temporarily shut off (the inspector must not adjust valves), the nozzles are plugged. Static pressure drop across each stage should be recorded, if possible, to help in problem diagnosis.

To complete the check of the water system, the inspector should measure the temperature and the pH of the sump liquor. It is advisable to take a liquor sample; however, the expense should not be incurred unless there are reasons to suspect operational and/or corrosion problems (chain-of-custody procedures must be followed). During the inspection, the integrities of the scrubber shell and the component parts should be rountinely checked.

4.4.3 Electrostatic Precipitators

There are four problems which can affect the performance of an ESP:

- 1. Electrical,
- 2. Gas flow,
- 3. Mechanical, and
- 4. Effluent.

In each problem category, there are three to five symptoms which occur with reasonable frequency, but the observed symptoms do not often indicate a particular problem. Due to the complexity caused by the interfacing of these problems, it is important that the inspector use a combination of symptoms in identifying operational difficulties.

The checklist (Table 7) and the flowsheet (Figure 8) are logical approaches to the evaluation of an ESP. Unlike the comparable charts for fabric filters and wet scrubbers, those for an ESP include a preliminary flowcharting step for use if a diagram is not available, so that the electrical data can be simplified and understood.

The inspector should begin in the main control room (or the substation) where much of the electrical data can be obtained. Performance evaluation should include, but not necessarily be limited to:

- 1. Power density calculations,
- 2. Evaluation of parallel field secondary currents,
- 3. Evaluation of inlet field secondary currents,
- 4. Spark rate,
- 5. Hopper heater/vibrator operational status,
- 6. Penthouse purge fan operational status,
- 7. Hopper unloading frequency,
- 8. Rapper operational status, and
- 9. Rapper frequency in various locations.

We recommend that internal ESP inspections be done only when the inspector is accompanied by a company representative. Furthermore, the inspector should always wear a respirator, hardhat, and gloves; should fully understand the lockout procedures used at the plant, and should strictly adhere to safety procedures due to the many potential hazards. A precipitator is essentially a giant capacitor.

Inside the unit, it is possible to identify many operating problems which are hard to diagnose otherwise. Particular attention should be given to:

- Dust accumulation on turning vanes and distribution plates which can indicate and/or cause poor gas distribution and low particulate control efficiency;
- Obvious corrosion which suggests in-leakage of air or operating below the acid dewpoint;
- A full hopper which causes misalignment of the collection plates, which in turn can reduce collection efficiency;
- 4. Removal of a large number of discharge wires in a bus section which can indicate alignment problems and/or design deficiences; and
- 5. Inadequate rapping of collection plates, and/or discharge wire.

Broken discharge wires can generally be located by checking for bottle weights hanging below the normal level.

At the end of step 4, the inspector decides whether or not the ventilation system and the process, itself, need to be inspected. If the operation and maintenance of the control system appear to be adequate <u>and</u> if there are no indications of changes in effluent characteristics (e.g., increased gas flow rates, smaller particle size distribution, higher temperature), the inspection should be terminated. Otherwise, the ventilation system (if applicable) and the process operations should be visited.

4.5 STEP 5: CHECK THE VENTILATION SYSTEM

To inspect the ventilation system, the inspector checks the capture velocities of hoods to the extent possible using the velometer. Factors which could cause inadequate capture efficiency include the following problems (partial list):

- 1. Inadequate hood design and location,
- 2. Thermal drafts,
- 3. Cross-drafts in the vicinity of the hood, and
- 4. Leaking of air into hoods and/or ducts within the system.

If the ductwork is accessible, the static pressures at various points should be inspected; furthermore, the physical conditions of ducts should be observed to locate leaks. Improper hood locations can account for drops in pollutant mass loading or for changes in particle size distributions. Releases of emissions to roof monitors or as fugitive material should be checked, especially for movable hoods.

4.6 STEP 6: EVALUATE PROCESS OPERATING CONDITIONS

The purpose of the process inspection is to answer questions and to confirm conclusions reached in earlier steps.

However, if the source is subject to special state/local regulations or to New Source Performance Standards or to National Emission Standards for Hazardous Air Pollutants, compliance with recordkeeping and monitoring requirements should be checked first, using a DSSE-published series of documents which includes checklists and associated information.

The inspector can seek answers to questions which were derived from steps 1 through 5. The inspector addresses problems which could be individually or collectively responsible for nonoptimal performance, including, but not limited to:

1. Has the production rate increased (higher mass loading and/or gas flow rate)?

- 2. Have the raw materials and/or fuels changed to the extent that effluent characteristics are different?
- 3. Has the process equipment deteriorated to the extent that emissions are affected?
- 4. Have changes in operating conditions resulted in more difficult collection problems (particle size decreases)?

The process inspector should begin at the control centers where process monitors are located to look for signs of changes in operating conditions and to observe current operating/mainte-nance practices. At these centers, process operating data are available; a process flowsheet is generally posted on the control panel; plant operators are generally nearby; and the subdued noise level is conducive to technical discussions.

While in the control room, the inspector should seek out the process monitors and/or records most pertinent to the compliance questions. Example "inspection points" for six source.types are in Table 2; several generalizations can be drawn from this table.

- In most cases, the inspector can confirm increased production rate by using data available in the control room;
- 2. The inspector can confirm raw material changes by inspecting records kept either in the control room or in the administrative offices:
- 3. The inspector cannot easily confirm process operational changes;
- 4. For batch operations, it is necessary to observe the equipment since little useful information is available in the control room; and
- 5. For other processes, it is possible to identify changes in operating conditions, but the significance of the changes is hard to determine.

Follow-up questions remaining after the inspection of records and monitors in the control room can be quite time consuming due to the cyclic processes and to distances between inspection

points at large plants. The follow-up can be guided by the items listed in Table 8, but the inspector is encouraged to develop more extensive lists for specific plants. The presence of fugitive emissions should be noted.

TABLE 8. EXAMPLE INSPECTION POINTS, COUNTERFLOW INSPECTION PROCEDURES

Type of Industry/Sourc	Inspection in the e Office and/or Control Room	Inspection of Specific Equipment
1. Confirm th	e Rates of Production and/or Generation	
Sulfuric acid	Check acid production records, and observe acid flow rate indicator.	N/A
Asphalt	N/A	Observe number of batches shipped per hour of plant operation.
Utility or industrial boiler	Check megawatt generation and steam production rates.	N/A
Cement	Check raw material feed rate records.	n/A
Refinery	Check throughput records on catalytic cracker.	N/A
2. Confirm Ra	w Material Changes	
Asphalt	N/A	Perform lab tests to determine coal gradation and surface moisture percentage.
Utility or industrial boiler	Check daily records of analyses: %% ash, %%% Btu content, ash fusion temp.	Take sample for later analyses.
Sulfuric acid	Check records of feed content; high levels contribute acid mist.	N/A
Refinery	Check production inventory records.	3/A

TABLE 8 (Continued)

Type of Industry/Source	Inspection in the e Office and/or Control Room	Inspection of Specific Equipment					
3. Confirm Pr	oceds Operational Changes	Sympton					
Sulfuric acid	Check catalyst bed temp and air flow rate to catalyst bed if SO ₂ monitor values are high. Check acid concentration temp and flow to absorbers.	N/A					
Secondary brass and bronze	Check records for percentage of zinc in alloy and for pouring temp.	Check for grease and oil on scrap an for operational practices such as maintenance integrity of slag load. Check hood caption velocity in furnace area. Determine if zinc is added before furnace temp is maximum					
Utility or industrial boiler	Check air preheater exit temperatures.	n/a					
4. Confirm Pr	ocess Equipment Deterioration						
Sulfuric acid	Observe SO ₂ concentration monitors; check for inactive or poisoned catalyst if SO ₂ is high.	Check pressure drop across mist eliminator. If low, check for shortcircuiting; if high, check for plugging.					
Secondary brass and bronze	N/A	Check hoods and ductwork for physical damage and caption velocity					
Utility or industrial boiler	Check excess air level by means of 0_2 readings.	Check to see if stoker boiler draft above fuel beds has >0.10" negative pressure.					
Refinery	N/A	Observe flow rate.					

SECTION 5

POST-INSPECTION

5.1 PLANT INTERVIEW

Having evaluated the exhaust system, monitoring equipment, control systems, and possibly the process itself, the inspector should meet—with a responsible plant official to:

- Ask follow-up questions as necessary,
- 2. Review inspection notes so that there is general agreement on the technical facts, and
- 3. Discuss need for followup inspection or additional records.

5.2 FILE UPDATE AND REPORT PREPARATION

All appropriate file entries should be changed as necessary. The conclusions of the inspector, based on observations and calculations, should be clearly stated in a concise paragraph in the inspection report which should also include two sheets—the control device diagnostic checklist and a coverpage (Table 9)—with the following information:

- -Any change in responsible plant personnel,
- -Requested permit changes or reported process modifica tions,
- -Results of Counterflow evaluation,
- -Action requested,
- -Inspector's signature, and
- -Date of inspection.

A copy of both sheets should be kept in the inspector's source file and in the agency's central file.

SECTION 6

SAFETY CONSIDERATIONS

The field inspector should take any precautions necessary to absolutely ensure that the inspection is conducted safely. All applicable OSHA regulations should be satisfied. If there is any question whether all or part of the inspection can be done safely, that part should be delayed until the issue is adequately resolved.

There are several principles which should be obeyed during a field inspection, namely:

- Prior to the inspection, the files should be reviewed to assess possible hazards. Consult references, such as the Pocket Guide of Industrial Hazards and Occupational Diseases, a Guide to Their Recognition;
- The inspection should bring all necessary safety equipment (in good working order);
- 3. Safety equipment should be worn whenever necessary regardless of the practices of plant personnel;
- 4. The inspector should proceed with the inspection at a controlled pace so there is time to fully assess possible hazards and so foolish accidents do not occur;
- 5. Inspectors should not work alone. If plant personnel are not available or willing to accompany the inspector, then the inspector should wait until additional help is available from the agency or the company;
- 6. Prior to any confined space entry, the inspector should read Appendix C, and follow the recommendations completely;

- 7. Physical examinations should be completed annually;
- 8. Accidents should be reported to supervisory personnel immediately, regardless of the suspected severity of the injury;
- 9. Lock-out procedures should be followed completely;
- 10. Entry to electrostatic precipitators should not be done until grounding hooks have been used in all areas to be inspected;
- 11. Hoppers full of material should never be opened or entered by the inspector; and
- 12. Fans vibrating severely should be avoided and plant personnel should be notified immediately.

A field inspector cannot afford to under-estimate potential hazards. The inspector is inherently exposed on a regular basis to a wide variety of hazards and does not have the opportunity to acquaint himself or herself with the details of each plant. For these reasons, it is particularly important that the inspector adhere to the basic principles outlined above. It should also be realized that these are simply a starting point and other precautions will be needed in most circumstances.

REPORT PLANT I.D.		REPORT NUMBER
SPECIAL ACTION RECOMMENDED (Yes) (No) I. GENERAL INFORMATION A. Sources Inspected Production Status B. Reasons for Inspection (Check Appropriate Items) Routine Inspection Compliance Progress Complaint Investigation Permit Review/Renewal Stack Testing Observed Tax Certification Special Studies Emergency Episode Other Equipment Malfunction C. Plant Representative Contacted (Name and Title) D. Inspection Procedures and Conditions Prior Notice (Check One) Yes No Time/Date Duration On-Site Type Inspection (Check One) Counterflow Follow-Up Other	INSPECTION	PLANT NAME
I. GENERAL INFORMATION A. Sources Inspected Production Status B. Reasons for Inspection (Check Appropriate Items) Routine Inspection Compliance Progress Complaint Investigation Permit Review/Renewal Stack Testing Observed Tax Certification Special Studies Emergency Episode Other Equipment Malfunction C. Plant Representative Contacted (Name and Title) D. Inspection Procedures and Conditions Prior Notice (Check One) Yes No Time/Date Duration On-Site Type Inspection (Check One) Counterflow Follow-Up Other	REPORT	PLANT I.D.
A. Sources Inspected Production Status		SPECIAL ACTION RECOMMENDED (Yes) (No)
B. Reasons for Inspection (Check Appropriate Items) Routine Inspection Compliance Progress	I. GENERAL INFORMATION	
Routine Inspection Compliance Progress Complaint Investigation Permit Review/Renewal Stack Testing Observed Tax Certification Special Studies Emergency Episode Other Equipment Malfunction C. Plant Representative Contacted (Name and Title) C. Plant Representative Contacted (Name and Title) C. Inspection Procedures and Conditions Prior Notice (Check One) Yes No Time/Date Duration On-Site Type Inspection (Check One) Counterflow Follow-Up Other	A. Sources Inspected	Production Status
Routine Inspection Compliance Progress Complaint Investigation Permit Review/Renewal Stack Testing Observed Tax Certification Special Studies Emergency Episode Other Equipment Malfunction C. Plant Representative Contacted (Name and Title) D. Inspection Procedures and Conditions No Time/Date Duration On-Site Type Inspection (Check One) Counterflow Follow-Up Other		-
C. Plant Representative Contacted (Name and Title) D. Inspection Procedures and Conditions Prior Notice (Check One) Yes No Time/Date Duration On-Site Type Inspection (Check One) Counterflow Follow-Up Other	•	
C. Plant Representative Contacted (Name and Title) D. Inspection Procedures and Conditions Prior Notice (Check One) Yes No Time/Date Duration On-Site Type Inspection (Check One) Counterflow Follow-Up Other	Routine Inspection	Compliance Progress
C. Plant Representative Contacted (Name and Title) D. Inspection Procedures and Conditions Prior Notice (Check One) Yes No Time/Date Duration On-Site Type Inspection (Check One) Counterflow Follow-Up Other	Complaint Investigation	Permit Review/Renewal
C. Plant Representative Contacted (Name and Title) D. Inspection Procedures and Conditions Prior Notice (Check One) Yes No Time/Date Duration On-Site Type Inspection (Check One) Counterflow Follow-Up Other	Stack Testing Observed	Tax Certification
C. Plant Representative Contacted (Name and Title) D. Inspection Procedures and Conditions Prior Notice (Check One) Yes No Time/Date Duration On-Site Type Inspection (Check One) Counterflow Follow-Up Other	Other	Emergency Episode
Time/Date Duration On-Site Type Inspection (Check One) Counterflow Follow-Up Other	D. Inspection Procedures and Conditions	s
Type Inspection (Check One) Counterflow Follow-Up Other		
Other	Time/Date Durat:	ion On-Site
	Type Inspection (Check One) Counter	rflow Follow-Up
Weather Wind Direction	Other	
	Weather	Wind Direction
II. PRE-INSPECTION INTERVIEW	II. PRE-INSPECTION INTERVIEW	•
A. Production Status: Normal Abnormal		Abnormal
A. Production Status: Normal Abnormal B. Control Equipment: Normal Abnormal C. Permit/Compliance Schedule Changes Needed: Yes No D. Comments	A. Production Status: Normal	Abnormal

(continued)

•	Report	Number	
II. INSPECTION RESULTS		•	
. General Conclusions		•	
All Sources in Compliance	e with:		
Mass Emission Regulation	ons: Yes	No	N/A
Visible Emission Regula	ations: Yes	No	N/A
Fuel Quality Regulation	is: Yes	No	N/A
Continuous Monitoring R Sampling/Testing Requir	(egulations: Yes	No	N/A
Recordkeeping Requireme	ements: les	NO	N/A
Permit Stipulations:	Yes —	No	N/A N/A
Special Orders:	Yes	No	N/A
OWM Practices: Good	A110#888	Pa	
Housekeeping: Good	Average Average	Por	~
	werage		
Specific Conclusions			
Compliance Questionable D	Due To:		
Changes in Raw Material	ls and/or Fuels		
Production Rates Increa	ases		
Operational Changes in	Process		
Deterioration of Proces	ss Equipment		
Operational Problems in	n Control Equipment	(Check Approp	riate Items Below)
Electrostatic	Fabric	Wet	
Precipitators	<u>Filters</u> .	<u>Scrubbers</u>	
Resistivity	Tears/Pinholes	Low Liquor	Flow
Resistivity	Blinding	Gas Flow R	ate Low
TR Sets	Blinding	Gas Flow R	ate Low
TR Sers Insulators Discharge Wires	Blinding Bleeding Cleaning System	Gas Flow R Bed Pluggi Nozzle Ero	ate Low ng sion
TR Sers Insulators Discharge Wires	Blinding Bleeding Cleaning System	Gas Flow R Bed Pluggi Nozzle Ero	ate Low ng sion
TR Sets Insulators Discharge Wires High Velocity Gas Distribution	Blinding Bleeding Cleaning System	Gas Flow R Bed Pluggi Nozzle Ero Demisters Throat Adj	ate Lowsion
TR Sets Insulators Discharge Wires High Velocity Gas Distribution Rappers	Blinding Bleeding Cleaning System Hopper Overflow Corrosion	Gas Flow R Bed Pluggi Nozzle Ero Demisters Throat Adj Tray Colla	ate Low ng sion ustment
TR Sets Insulators Discharge Wires High Velocity Gas Distribution Rappers Solids Handling	Blinding Bleeding Cleaning System Hopper Overflow Corrosion	Gas Flow R Bed Pluggi Nozzle Ero Demisters Throat Adj Tray Colla	ate Lowsion
TR Sets Insulators Discharge Wires High Velocity Gas Distribution Rappers Solids Handling Plate Warpage	Blinding Bleeding Cleaning System Hopper Overflow Corrosion	Gas Flow R Bed Pluggi Nozzle Ero Demisters Throat Adj Tray Colla	ate Low ng sion ustment
TR Sets Insulators Discharge Wires High Velocity Gas Distribution Rappers Solids Handling	Blinding Bleeding Cleaning System Hopper Overflow Corrosion	Gas Flow R Bed Pluggi Nozzle Ero Demisters Throat Adj Tray Colla	ate Low ng sion ustment
TR Sets Insulators Discharge Wires High Velocity Gas Distribution Rappers Solids Handling Plate Warpage Mass Overload Other	Blinding Bleeding Cleaning System Hopper Overflow Corrosion	Gas Flow R Bed Pluggi Nozzle Ero Demisters Throat Adj Tray Colla	ate Low ng sion ustment
TR Sets Insulators Discharge Wires High Velocity Gas Distribution Rappers Solids Handling Plate Warpage Mass Overload Other	Blinding Bleeding Cleaning System Hopper Overflow Corrosion	Gas Flow R Bed Pluggi Nozzle Ero Demisters Throat Adj Tray Colla	ate Low ng sion ustment
TR Sets Insulators Discharge Wires High Velocity Gas Distribution Rappers Solids Handling Plate Warpage Mass Overload Other	Blinding Bleeding Cleaning System Hopper Overflow Corrosion	Gas Flow R Bed Pluggi Nozzle Ero Demisters Throat Adj Tray Colla	ate Low ng sion ustment
TR Sets Insulators Discharge Wires High Velocity Gas Distribution Rappers Solids Handling Plate Warpage Mass Overload Other	Blinding Bleeding Cleaning System Hopper Overflow Corrosion	Gas Flow R Bed Pluggi Nozzle Ero Demisters Throat Adj Tray Colla	ate Low ng sion ustment
TR Sets Insulators Discharge Wires High Velocity Gas Distribution Rappers Solids Handling Plate Warpage Mass Overload Other	Blinding Bleeding Cleaning System Hopper Overflow Corrosion	Gas Flow R Bed Pluggi Nozzle Ero Demisters Throat Adj Tray Colla	ate Low ng sion ustment
TR Sets Insulators Discharge Wires High Velocity Gas Distribution Rappers Solids Handling Plate Warpage Mass Overload Other Samples Taken (Describe)	Blinding Bleeding Cleaning System Hopper Overflow Corrosion	Gas Flow R. Bed Pluggi Nozzle Ero Demisters Throat Adj Tray Colla Corrosion	ate Low
Insulators Discharge Wires High Velocity Gas Distribution Rappers Solids Handling Plate Warpage Mass Overload Other Samples Taken (Describe)	Blinding Bleeding Cleaning System Hopper Overflow Corrosion	Gas Flow R. Bed Pluggi Nozzle Ero Demisters Throat Adj Tray Colla Corrosion	ate Low
TR Sets Insulators Discharge Wires High Velocity Gas Distribution Rappers Solids Handling Plate Warpage Mass Overload Other Samples Taken (Describe)	Blinding Bleeding Cleaning System Hopper Overflow Corrosion	Gas Flow R. Bed Pluggi Nozzle Ero Demisters Throat Adj Tray Colla Corrosion	ate Low
TR Sets Insulators Discharge Wires High Velocity Gas Distribution Rappers Solids Handling Plate Warpage Mass Overload Other Samples Taken (Describe)	Blinding Bleeding Cleaning System Hopper Overflow Corrosion	Gas Flow R. Bed Pluggi Nozzle Ero Demisters Throat Adj Tray Colla Corrosion	ate Low
TR Sets Insulators Discharge Wires High Velocity Gas Distribution Rappers Solids Handling Plate Warpage Mass Overload	Blinding Bleeding Cleaning System Hopper Overflow Corrosion	Gas Flow R. Bed Pluggi Nozzle Ero Demisters Throat Adj Tray Colla Corrosion	ate Low
TR Sets Insulators Discharge Wires High Velocity Gas Distribution Rappers Solids Handling Plate Warpage Mass Overload Other Samples Taken (Describe)	Blinding Bleeding Cleaning System Hopper Overflow Corrosion	Gas Flow R Bed Pluggi Nozzle Ero Demisters Throat Adj Tray Colla Corrosion	ate Low

APPENDIX A (See Working File Handout)

APPENDIX B (Sample Inspection Data Sheets)

A. INSPECTION INFORMATION

1.	IDENTIFICATION
	Company
	Plant Name
	Plant I.D. Number
	Address
	Control Device/System Number
	Process Served_
2.	PROCEDURES AND CONDITIONS
	Prior Notice: Yes No Time(s) On-Site
	Type Inspection
	Inspectors
	Plant Representatives
	Information Claimed Confidential: YesNo

В.		ble Emissions ervations	Inspection No									
			Confidential:									
			Page No									
	1.	STACK CHARACTERISTICS										
	٠.											
		Location										
		Height	······································									
		Temperature										
		Exit Dimensions										
		Orientat i on	·									
		Other Information										
		• }										
	2.	STACK EFFLUENT										
		Detached Plume: NoYes	s Distance									
		Color										
		Puffing: Yes	No									
		Opacity										
	Tim	e Average Opacity	Observation Point	oint Sh								
												
	3.	FUGITIVE EMISSIONS										
		Control Device: YesNo	•									
		Solids Removal System: Yes_										
		Process: YesNo										
		Continuous	Intermittent									
		Adiacent Deposits: Yes										

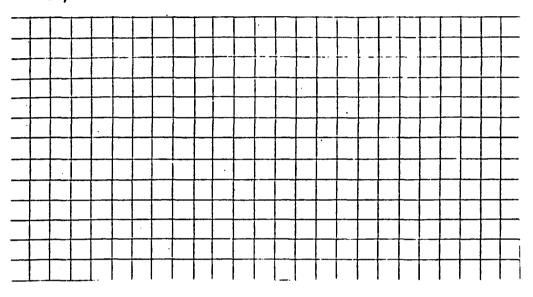
C. Fan	Data	Inspection No											
			Equipment No										
			Confidential: YesNo_										
		·	Page No of										
	1.	FAN MOTOR											
		Manufacturer											
		Model No	Type										
			Maximum Amps										
			Service factor										
		Operating Current: Panel											
		- }											
	2.	DRIVE											
	DirectBelt	Other											
		Sheath Reduction_											
			No										
	3.	FAN											
		Manufacturer											
		Model No.	Type										
		Fan Vibration											
		Gas Temperature at inlet, OF											
		Ean D D M											
		Fan Static Pressures: Inlet	Outlet										
			MeasuredPanel										
		Fan Housing Condition											
		Dampers											
		For Fuit											

D.	.Electrostatic Precipitator Data								Inspection No Equipment No Confidential: YesNo												_				
																									_
	1.	DESCRIPTIVE INFORMATION																							
		Type_																							_
																									_
	Manufacturer Model Number																						_		
		Plant	: Ir	ivei	ntor	~y N	lumb	er																	_
		Plant Inventory Number Date Installed															-								
		Numbe	er c	of (Chan	nber	·s																		
		Numbe	r c	of I	Fiel	lds	in	Sei	rie	S,		•													
		Number of Chambers Number of Fields in Series Specific Collection Area (Ft²/1000 Ft³)														-									
		Design Superficial Viscosity (Ft/Sec)															_								
	Pulse Energization (Yes/No)																								
	ruise Energization (res/No)														_										
	2. LOCATION																								
		Building/Area																							
		Eleva																							
		2.010					-																		-
	3.	LAYOU	IT (SKE	ETCH	ł FI	ELD	L/	OY <i>P</i>	UT	AN	D N	IUM	BEF	R F	IEI	_DS	, 9	SHO	W F	AN	S)			
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E.	Electrost	tatic	Precipitator
•	External	Inspe	ection

Inspection No			
Equipment No			
Confidential:	Yes	No	
Page No.	of		

HOPPER LAYOUT (SKETCH TOP VIEW AND NUMBER; SHOW SOLIDS HANDLING SYSTEM)



2. HOPPER DESCRIPTION

Vibrators: Yes	NoNoNo		
Heaters: Yes			
Insulation: Yes			
Level Indicators: Yes	No		
Physical Condition (Characterize)		
Transport Equipment: Screws	Pneumatic_	Other	
Transport Equipment Operating:	Yes	No	
Characterize Discharge			

E.	Electrosi	tatic	Precipitat	or
	External	Inspe	ection	

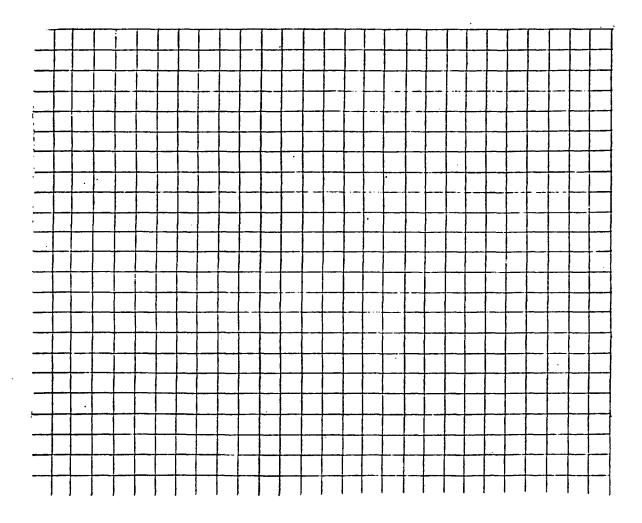
Inspection No.	
Equipment No	
Confidential:	Yes No
Page No	of

3. HOPPER VALVES

Type:	Screw	Other
Speed/	Cycle Times	

Blade 1	Туре	

4. RAPPER LAYOUT (SKETCH TOP VIEW, SHOW DISCHARGE WIRE UNITS AS D, COLLECTION PLATE UNITS AS C AND DISTRIBUTION PLATE UNITS AS X).



Ε.	Electrostatic	Precipitator
	External Inspe	ection

Inspection No.		
Equipment No		
Confidential:	Yes	No
Page No.	of	

5. RAPPER PERFORMANCE (Continued)

COLLECTION PLATE RAPPERS

No.	Time Interval (Minutes)	Duration (Seconds)	Comments
C ₁			
C ₂			
C ₃			
C4			
C ₅			
C ₆			
C7 .		,	
C ₈			
C, _			
C10		` .	
C11			
C12 _			
C ₁₃			
C14			
C ₁₅		·	
C ₁₆		,	
C ₁₇			
C18			
C19			
C20			

E.	Electrost	tatic	Precip	itator
	External	Inspe	ction	

Inspection No.		
Equipment No		
Confidential:	Yes	No
Page No.	of	

5. RAPPER PERFORMANCE

DISCHARGE WIRE RAPPERS

	DISCHARGE WIRE TOUTENS				
No.	Time Interval (Minutes)	Duration (Seconds)	Comments		
D_1					
D ₂					
D3					
D4					
Ds					
D ₆					
D ₇					
D ₈					
D ₉					
D ₁₀	·				
D ₁₁					
D ₁₂	·				
D ₁₃					
D ₁₄					
D ₁₅					
D ₁₆					
D ₁₇					
D ₁₈					
D ₁₉					
D ₂₀	·				

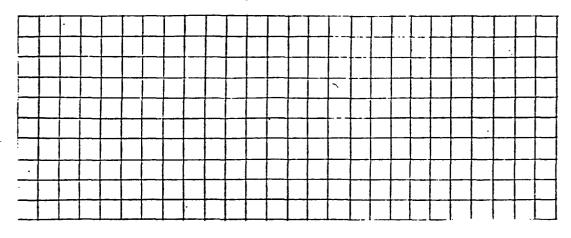
	Electrostatic Precipitator External Inspection		Inspection NoEquipment No								
				1: Yes No							
				of							
5.		ER PERFORMANCE (Contin	•								
	No.	Time Interval (Minutes)	Duration (Seconds)	Comments							
	X ₁										
	X 3 X 4										
	X ₅										
6.		ER DESCRIPTION HARGE WIRES Type									
		Number Manufacturer Air Pressure									
	COLL	ECTION PLATES Type									
		Number									
	DICT	ManufacturerAir Pressure									
	121	RIBUTION PLATES Type									
		Number									
		Air Pressure ·									

E.	Electros	tatic	Precipitate	or
	External	Inspe	ction	

T-R10

Inspection No.		
Equipment No		·
Confidential:	Yes	No
Page No.	of	

7. TRANSFORMER - RECTIFIER SET LAYOUT (SKETCH TOP VIEW SHOWING T-R SETS ON CHAMBERS AND FIELDS)



8. TRANSFORMER - RECTIFIER SET DESCRIPTION

Power Control: Yes____No___ Mode Voltage Current Spark Rate Plant Milliamp Model Manufacturer Rating Туре No. No. No. T-R₁ T-R₂ T-R₃ T-R4 T-R₅ T-R₆ T-R7 T-R₈ T-R₉

E.Electrost	tatic	Precipitat	cor
External	Inspe	ection	

Inspection No.		
Equipment No		
Confidential:	Yes	No
Page No.	of	

9. TRANSFORMER - RECTIFIER SET CONDITIONS

No.	Primary current (amperes)	Primary voltage (volts)	Secondary current (milliamps)	Secondary voltage (kilovolts)	Spark rate #/min	Control mode M-manual A-automatic
T-R-1a						
T-R-1b						
T-R-2a						
T-R-2b						
T-R-3a						
T-R-3b						
T-R-4a						
T-R-4b						
T-R-5a						
T-R-5b	 					
T-R-6a						
T-R-6b						
T-R-7a						
T-R-7b						
T-R-8a						
T-R-8b						
T-R-9a						
T-R-9b						
T-R-10a						
T-R-10b						

E.		ctrostatic Precipitator	Inspection No.												
	EXLE	ernal Inspection	Equipment No												
			Confidential: YesNo												
			Page No of												
	10.	OPERATING INFORMATION													
		Gas Inlet Temperature, OF													
			ator Lights (Identify units not on)												
		Penthouse Heater/Blower Operational Indicator Lights (Identify unit not on)													
	11.	OPACITY MONITORS													
		Opacity - Minimum, %													
		Average, %													
		Maximum, %													
		•	Duration, Intensity)												
		Calibration Spikes (Characterize	e Levels, Frequency)												
		Comments													
		•													

F. Electrosi Interal				рт	iato	or						Eq	spo ui nf	pme	ent	No	·_							-
												Pa	ge	No)			01	f _			-		
1.	PURPOSE																							
	Reason(s) Necessary																							
٠					··-															 : 				
	SAFET	Y EV	ALUAT	ION	I																			
	Lockout Procedure Followed																							
	Plant Employee Performing Lockout															lo.								
		Grounding Straps Available: YesNoNoNo																						
	Purge																							
	02, %																							
	Combu	stib]	les,	%																				
	Noise																							
	NoiseOther																							
															11 -									
	Other Inspe				ndı	ıct	ed	Du	e ·	to	Pot	ten	t1a	3	на	2d f	`as	(Ch	ara	ct	er	ize)
					ndı	ıct —	ed	Du	e .	to 	Pot	ten —	t16	a I	на	2 d f	`as	(Ch	ara 		er	ize	
					ndı	ıct	ed	Du	e .	to	Pot	ten —	t16		на		`ds	(Ch	ara	ct	er	ize)
2,	Inspe	ctior ———	Not	Co																			ize)
2,		ctior ———	Not	Co																			ize)
2.	Inspe	ctior ———	Not	Co																			ze)
2,	Inspe	ctior ———	Not	Co																			ze)
2,	Inspe	ctior ———	Not	Co																			ze)
2,	Inspe	ctior ———	Not	Co																			ze)
2,	Inspe	ctior ———	Not	Co																			ize)
2,	Inspe	ctior ———	Not	Co																			ze	
2,	Inspe	ctior ———	Not	Co																			ize	
2,	Inspe	ctior ———	Not	Co																			ize	
2,	Inspe	ctior ———	Not	Co																			ize	

F.	Elec Inte	trostatic Precipitator rnal Inspection	Inspection No. Equipment No.		
			Confidential:		
			Page of		
	3.	HATCH CONDITIONS			
		Gaskets			
		Corrosion_			
			_		
	4.	PENTHOUSE CONDITIONS			
		Purge Air		•	
		Heater(s)			
		Insulators			
		Alignment of Collection Plates			
		Comments			

F.	Elec	trostatic Precipitator	Inspection No				
	Inte	rnal Inspection	Equipment No	***			
			Confidential:				
			Page No				
	5.	ELECTRODE CONDITIONS					
		DISCHARGE WIRES					
		Туре					
		Diameter					
		Material					
		Spacing and Length					
		Conditions					
					·		
		COLLECTION PLATES					
		Type					
		Material					
		Spacing and Length					
		Conditions		 			
							
		Alignment					

F.	Elec Inte	trostatic Precipitator rnal Inspection	Inspection No. Equipment No.		
			Confidential:		
	 Inter 7. 	•	Page No	of	
	6.	INTERNAL SUPPORTS			
		Describe		 	
		Conditions			
			 		
	7.	GAS DISTRIBUTION EQUIPMENT			
		Type			
		Condition		17	
	g	HOPPERS			
	0.	Baffle Condition			
		Durite Condition			
		Hopper Condition_			

G.	Continuous	Monitor	Evaluation

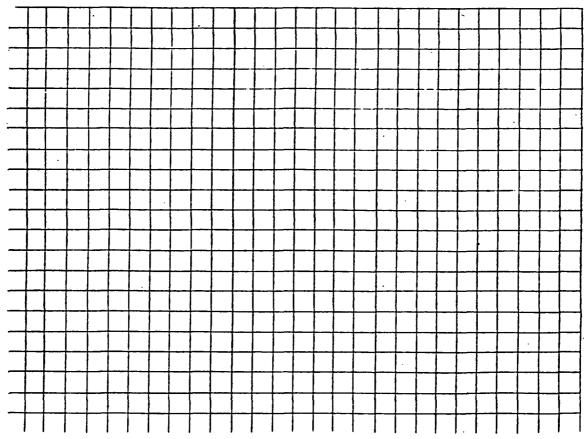
Inspection No.		
Equipment No		
Confidential:	Yes	No
Page No	of	

1. DESCRIPTIVE DATA

Manufacturer	
Model	
Туре	
Date Installed	
Single or Multiple Breeching	
NSPS Applicable: Yes	No

2. TRANSMISSOMETER

LAYOUT (SHOW LOCATION RELATIVE TO FLOW RESTRICTIONS)



G. Cont	tinuous Monitor Evaluation	Inspection No. Equipment No. Confidential: Page No.	YesNo	
2.	TRANSMISSOMETER (Continued)			
	Approximate Path Length, (Feet)			
	Vibration (Characterize)			
	Housing (Characterize)			
	Purge Air (Condition of Blowers an			
	Filters (Characterize Type and Des			
	Alignment (Window Check)			
3.	CONSOLES			
	Breeching/Stack Correlation			
	Zero/Span			
	Comments			
.i				

H.	Elec Eval	trostatic Precipitator uation	Inspection No. Equipment No.		
			Confidential:		
		•	Page No	_ of	
	1.	FILES/ADMINISTRATIVE			
		Specification Sheets Available: Prints Available (Characterize)			
		Supervisor of Unit		· · · · · · · · · · · · · · · · · · ·	
		0 and M Personnel (Describe Staff		on)	
	2.	RECORDKEEPING		·· ·· · · · · · · · · · · · ·	·····
		Type Records			
		Operating Records (List Parameter			
		Diagnostic Records (Characterize)			
n	3.	PROCEDURES			
		Spare Parts Inventory (Characteria	ze)		
		004 03 (01		 	
		O&M Plan (Characterize)			
		Troubleshooting (Characterize)			

Samp	ples	Inspection NoEquipment No
		Confidential: Yes No_
		Page No of
•	Solids	
	Sample No	
	Location Obtained	
	Date/Time Obtained	·
	Results	
	·	
		· · · · · · · · · · · · · · · · · · ·
•	Other Samples	
	Sample No	
	Date/Time Obtained	
	Count	
•	Other	
	· · · · · · · · · · · · · · · · · · ·	

. Electros Evaluati	trostatic Precipitator Luation		Inspection No. Equipment No. Confidential:	Yes	No
			Page No	. ^{of}	
1. POW	ER INPUT				
Col	lection Plate Area	/Field			
	Inlet				
	Other_	- 	·.		
Dis	charge Wire Length	/Field			
	Inlet				
•	Other				
Field	Secondary Currents (Milliamps)	Power Input (Watts)		t Dens /Ft)	ities Watts/Ft²
1.	to the control of the control of				
2.	-				
3.					
4.	**************************************				
5.					
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10.					
11.	·				
12.	•				
13.	·				
14.	····			- 	
15.					

K.	2.			•	
			Confidential: Page No	Yes	No
	1.	PROCESS TYPE			
		Characterize Source	en e		
		Operating Schedule			
	•		•		
2.	2.	OPERATION			
		Product Type During Inspection			
		Production Data During Inspection_			
	1.	Fuels During Inspection_			
					

Sum	mary			Inspection No		
				Equipment No.		
		·		Confidential: YesNo		
				Page of		
1.	POWER INPL	JT				
2.						
8.	. ————		<u> </u>			
1.	EFFLUENT C	QUANTITY/CHARA		S		
5.	OTHER					
5.	SHEETS				-	
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	J	K	_			
Pre)				
	Date			· 		
Rev						
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A. INSPECTION INFORMATION

1.	IDENTIFICATION
	Company
	Plant Name
	Plant I.D. Number
	Address
	· ·
	Control Device/System Number_
	Process Served
2.	PROCEDURES AND CONDITIONS Prior Notice: Yes No Time(s) On-Site
	Type Inspection
	Inspectors
	Plant Representatives
	Information Claimed Confidential: YesNo

	Sible Emissions	inspection No.			
0bs	servations	Equipment No			
		Confidential: Yes			
		Page No of			
1.	STACK CHARACTERISTICS				
	Location				
	Height_				
	Temperature				
	Exit Dimensions				
	Orientation				
	Other Information	·			
	· .				
2.	STACK EFFLUENT				
	Detached Plume: NoYes	s Distance			
	Color				
	Puffing: Yes				
	Opacity				
<u>Ti</u>	ime Average Opacity	Observation Point	Sheet No.		
3.	FUGITIVE EMISSIONS				
	Control Device: Yes No)			
	Solids Removal System: Yes_				
	Process: Yes No				
	Continuous	Intermittent	····		
	Adjacent Deposits: Yes				

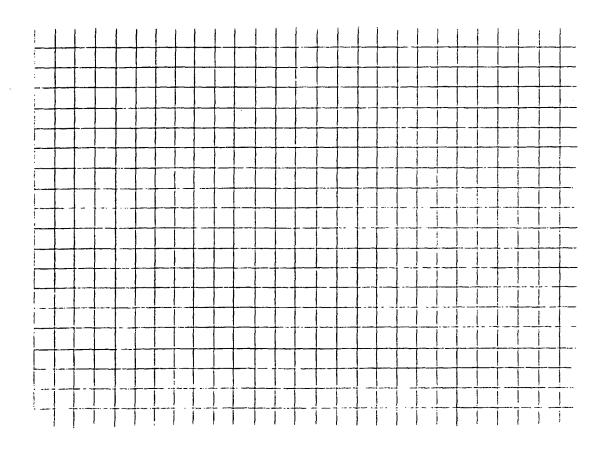
). F	an	Data	Inspection No
			Equipment No
			Confidential: Yes No_
		•	Page No of
1		FAN MOTOR	
		Manufacturer	
		Model No.	
		Rated Horsepower	
		Volts	
		Maximum R.P.M.	
		Operating Current: Panel	
		· .	
. 2		DRIVE	
		DirectBelt_	Other
		Audible Belt Slippage: Yes	No
3		FAN ·	
		Manufacturer	
		Model No.	Type
		Fan Vibration	
		Gas Temperature at inlet, ^o F	
		Fan R.P.M.	
		Fan Static Pressures: Inlet	Outlet
		Differential Static Pressures:	
		Fan Housing Condition	
		Dampers	
		Fan Fyit	

D. Fab	ric Filter Data			
		Confidential:	Yes _	No
1.	DESCRIPTIVE INFORMATION			
				
		Equipment No. Confidential: Yes No Page No of		
	Fabric Filter Type Manufacturer Model No. Plant Inventory No.			
	Date Installed			

2. LOCATION

Building/Area	
Inside	Outside

3. LAYOUT (SKETCH FABRIC FILTER, FAN, INLET, SOLIDS REMOVAL, ETC.).



ection	Equipment No. Confidential: Page No.	Yes	No
SOLIDS REMOVAL			
Valve Type: Rotary Fla Valve Speed/Frequency			
Transport Equipment: Screws			
Transport Equipment Operating: Ye			
Transport Equipment Discharging So Characterize Discharge			
Hopper Vibrators: Yes			
Hopper Insulation: Yes			
Hopper Level Indicators			
Hopper Condition			
Disposal Method			
SHELL CONDITIONS			
Insulated: Yes	No		
Possible Weld/Seam Gaps, Character	ize		
	· · · · · · · · · · · · · · · · · · ·	· · · · · · · · · · · · · · · · · · ·	

E. Fabric Filter External Inspection		Inspection No. Equipment No. Confidential: Yes Page No. of	 No
3.	OPERATING CONDITIONS		
	Static Pressure on Clean Side, Static Pressure on Dirty Side, On-site Monitor, Differential Tap Conditions Gas Inlet Temperature	Static Pressure	in. H ₂ C
4.	CLEANING SYSTEMS Type Frequency		
	Air Pressure, Drier: Yes Evidence of Water and/or Oil P	No	PSIG
5.	PRECLEANERS		
	Type		
	Static Pressures: Inlet Gas Inlet Temperature	Outlet	in. H ₂ O o _F

	ric Filter Internal pection			No
1.	PURPOSE			
	Reason(s) Necessary			
	Inventory Check Comprehensive Inspection Other			
	Safety Evaluation (Describe if a	nnlicable)		4*
	Respirator Necessary Temperature			
	- 1, 1 -			
	Combustibles			
	Electrical Grounding			
	Mechanical Hazards			
	Noise Other			
	. Inspection Conducted: Yes	No		
	Inspection Not Performed Due to			
2.	BAG LAYOUT (ATTACH DRAWING)			
	No. of bags			
	Length			f
	Diameter			i
	Material (Characterize)			
	Attachment(s)			

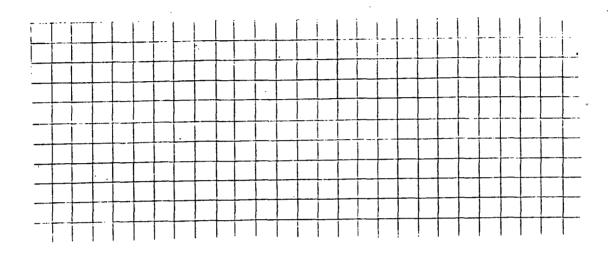
-		ric Filter Internal pection	Inspection No. Equipment No.		
		•	Confidential:		
			Page No.	of _	
	3.	HATCH CONDITIONS			
		Gaskets		 	
		Corrosion			
		Bolts/Ears			41
		Ease of Access			
	4.	LEAK JETS			
		Location			
		Number			
	5.	BAG CONDITIONS			

F.		bric Filter Internal spection				
			Confidential:			
			Page No.	of		
	6.	HOPPERS AND BLAST PLATES				
	7.	CLEANING APPARATUS				

ì	Samples		Inspection No.			
	·		Confidential: Page No.			
	1. SOL	.IDS DEPOSITS				
	Sam	nple No				
	Loc	ation Obtained		·		
	Dat	e/Time Obtained				
	Res	ults <u> </u>				
						
	2. FAB	RIC SAMPLES				
	Sam	ple No.				
	Loc	ation Obtained		- 		
	Dat	e/Time Obtained				
	•	Permeability				
	•	Tensile Strength		 		
		Count				
		Weight/Yard ²				
	3. OTH	IER				
	·					
					· · · · · · · · · · · · · · · · · · ·	
						

Inspection No.		·	
Equipment No.		·	
Confidential:	Yes _	No	
Page No.	of		

1. DUCTS (SHOW STATIC PRESSURES ON LAYOUT.)



2. HOOD

Configuration							
Average Capture Velocity							
Thermal Drafts (Characterize)							
Cross Currents (Characterize)							
Estimated Effectiveness	9/						

Proce	ess	Inspection No. Equipment No. Confidential: Page No.	Yes No	·
1.	PROCESS TYPE			
	Characterize Source	· · · · · · · · · · · · · · · · · · ·		
	Operating Schedule	•		
2.	OPERATION			
.	Product Type During Inspection			
	Production Rate During Inspection			
	Raw Materials During Inspection			
	Fuels During Inspection			

Page No.

Confidential: Equipment No. Inspection No.

Yes

Š

	Pos	sible Operating Problems	Average Baseline (Specify Value)	Observed (Specify Valu	Location* e)	Abnormal (Check)	Rating (1-10)	Recommended Action
******	D.	Cleaning System					•	
		 Filter house pressure high Pulse-jet air header p sure low Solenoids inoperative Reverse air fan inoperati Shaker motor inoperati Bag length long Equipment inaccessible High intensity cleaning required 	ntive N/A N/A N/A	N/A N/A N/A N/A	E E or I E or I E or I E or I E I E	ε	5 5 10 10 10 2 2 2 2	If sum (∑) of ratings is ≥10, perform internal inspection and check deposits on dirty side of bags. Check bag tension. Reschedule inspection in near future.
	Ε.	Hopper						
92		l. Filter house pressure drop high			E		5	If sum (Σ) of ratings is >10, perform internal inspection
		Solids-removal run in- termittent	N/A	N/A	, E		3	of hoppers.
		Indicator level exister and/or inoperative	nt <u>N/A</u>	N/A	E		2	
		4. Heaters nonexistent and inoperative	d/or N/A	N/A	E		2	
		5. Vibrators nonexistent and/or inoperative	N/A	N/A	E		2	
		6. Hopper valves corroded	N/A	N/A	1		3	
		7. Hopper slope <60 ⁰	N/A	N/A	E		2	
		8. Hoppers not insulated	<u> N/A</u>	N/A	E		2	
		9. Winter	N/A	. <u>N/A</u>	E		2	
		10. Hammer markings on hoppwalls	per <u>N/A</u>	N/A	E		2	
		11. Conveyor inoperative	N/A	N/A	E	Σ	= 10	,

*Location: E is external, and I is internal.

Pos	sible Operating Problems	Average Baseline (Specify Value)	Observed (Specify Valu	Location* e)	Abnormal (Check)	Rating (1-10)	Recommended Action
Α.	Bag Tears or Pinholes				······································		
	1. Filter house pressure			E		3	If sum (Σ) of ratings is > 10
	drop low (<80% avg.)		•			,	perform internal inspection.
	2. Opacity high			E		5	Check for deposits on fil-
	3. Bag age high (typical a			E		5	ter house clean side. Check
	4. Some bags inaccessible	N/A	N/A	Ţ		2	inaccessible bags. Use
	5. Design A/C high (>120%	·		E		4	fluorescent dye technique.
	6. Actual A/C high (>120%			E		4	Check integrity of fabric by
	7. Wear plate eroded	N/A	N/A	I		3	attempting to extend rips.
	8. Frequent high excursion	9		E or I		4	
					Σ) =	•
В.	Bag Blinding						
	1. Filter house pressure			E		7	If sum (Σ) of ratings is ≥ 10
	drop high (>150% avg.)						perform internal inspection.
	2. Opacity low			E		2	Check dirty side of bags for
	Cleaning frequency high (cycles/day)			E		5	coatings (this may be diffi- cult to identify in some
	4. Gas temp low (<20°F avg	1		E		4	cases). Check records for
	5. Moisture in gas stream	N/A	N/A	E		7.	steady rise in filter house
	6. Particulate sticky	N/A	$\frac{N/A}{N/A}$	Ē		4	pressure drop. Reschedule
	7. Air in-leakage (hoppers	/ N/A	N/A	ī		2	inspection in near future.
	access doors)	, <u>- 1715 </u>		•		-	inspection in hear ruture.
	8. Unit not insulated	N/A	N/A	E		2	
						. =	
c.	Bag Bleeding						
	l. Opacity high			E		5	If sum (Σ) of ratings is >10
	2. Pressure drop gradually	<u> </u>		E		2	attempt to confirm uses of
	increasing						fluorescent dye and black
	3. Cleaning frequency high			E		5	light.
	- · · · · ·					=	=

^{*}Location: E is external, and I is internal.

Summary						Inspection				
						Equipment				
						Confidenti				
						Page No	 ,	of _		
1.	CONTR	OL SY	STEM PE	RFORMANCE						
	Syste	m Air	Flow B	ased on Fan [Data _					AC
	Syste	m Air	Flow B	ased on Pitot	t Trav	erse				
	Syste	m Air	Flow B	ased on Proce	ess					_
	Actua	l Air	to Clo	th Ratio						_
	Desig	n Air	to Clo	th Ratio						
	Fabri	c Com	patibil	ity with Envi	ironme	nt				
										
2.	ADDIT	TONAL	COMMEN	TS						
٠.	NOOTI	TOWNE	COMMEN	13						
			<u> </u>							
						··				
										_
				·						
3.	SHEET	S INC	LUDED							
	Α		В	c	D.	[E	F		_
	G		н	I	J.	}	٠			
Pr	eparer:	Name				_ Signatur	^e			
Re	viewer:						^e			
Co	nies Rec			Initials						

Fabric Filter Supplemental	Inspection No.		
Information	Equipment No.		
	Confidential:	Yes	No
	Page No.	of _	

abric Filter Supplemental	Inspection No.	<u></u>				
nformation	Equipment No.	Equipment No.				
	Confidential:	Yes	No			

Page No. _____ of ___

LOCATION	DATA SHEET NO.
DESIGNATION	DATE
CLIENT	
PN	
CLAIMED CONFIDENTIAL Yes No _	·
A. DESCRIPTIVE INFORMATION	
Wet Scrubber Type	· · · · · · · · · · · · · · · · · · ·
Model Number	
Date Installed	
Process/Source Controll	ed
Particulate Characteris	tics
2. Demister:	
Cyclone	· · · · · · · · · · · · · · · · · · ·
Chevron	
Fiberous Mat	
Other	
3. Pumps:	
Number	
Recirculation	
Recirculation Pump Rated Horsepo	wer
Recirculation Pump	Type

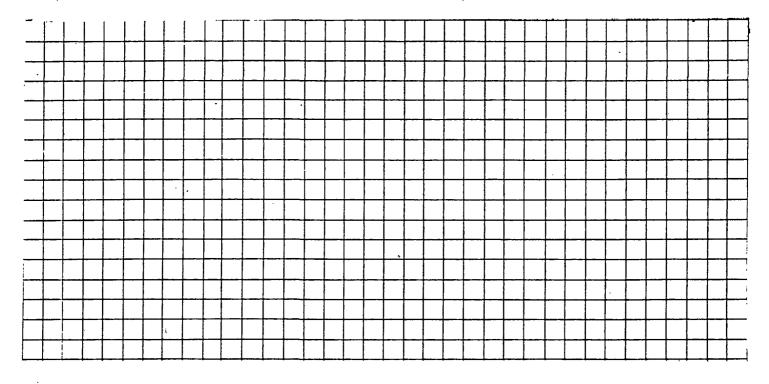
		Inspection No.
		Data Sheet No.
		Preparer
		Confidential: Yes No_
. COMP	ONENT INFORMATIO	N (continued)
4.	Fan/Motor (Spec	eify)
	Fan Manufacture	er
		dial Backward Forward
	Drive: Direct	Belt
	Damper Position	l
	Motor Manufactu	rer
	Rated Horsepowe	r
		ed Draft Induced Draft
5.	Instrumentation	(Check if Applicable)
	Differential	_,
	Pressures:	Throat
		Separator
		Demister
	Temperatures:	
		Gas Inlet
		Liquor Inlet
		Liquor Outlet
	pH:	Recirculation
		Exit Liquor
		Fan Motor Current
		Other
		Nozzle Pressure
	Flow Rates:	Recirculation
		Makeup
		Purge
	Motor Current:	Fan
		Pump

		ı	nspection No
		D	ata Sheet No.
		P	reparer
		c	onfidential: Yes No
в.	COME	PONENT INFORMATION (continued)
	6.	Materials of Construction (Specify type and gauge)
		Presaturator	
		Throat	
		Scrubber Shell	
		Trays/Bed Supports	
		Demister	
		Fan Housing	

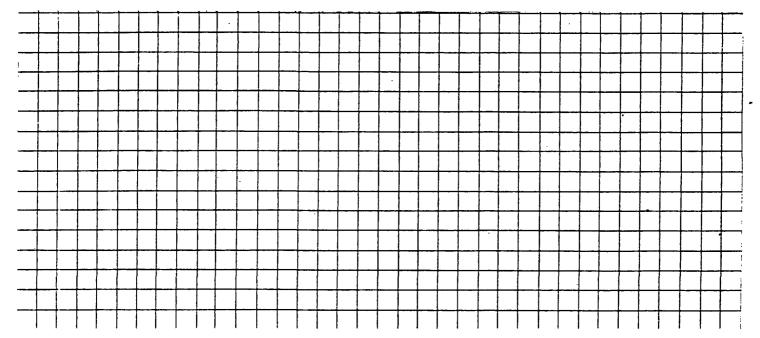
Inspe	ection	No.			-		
Data	Sheet	No.			-		
Preparer							
Confi	dentia	. 7 .	Voc	17			

C. DIAGRAM

Sketch wet scrubber system. (Show all major components and processes controlled.)



Sketch wet scrubber layout (each square l' x l')



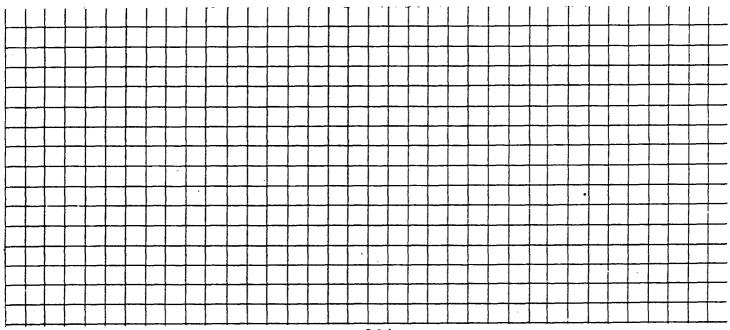
		Inspection No.				
				Sheet No.		
			Prepa	arer		
			Confi	idential:	Yes	No
F.	SAMPLE ANALYSIS					
	Scrubber Liquor Effl	uent				
	Sample No.				_	
	Location Obtain					
	Date/Time Obtai	ned			_	
	Results:					
	Suspended Solid	s			_ ppm	
	Dissolved Solid					
	рн	·		· · · · · · · · · · · · · · · · · · ·	-	
	Chloride				_ ppm	
	Scrubber Recirculation	on				
	Sample No.					
-	Location Obtain					
	Date/Time Obtain	ned			_	
	Results:					
	Suspended Solid	5			_ ppm	
	Dissolved Solid	5			ppm	
	рН				_	
	Chloride	-2			_ ppm	
	Other					
					_	
					_	
					_	
					_	
					-	
					_	

		Inspection No.				
		Data Sheet No.	,			
		Preparer				
		Confidential:				
CONTROL SY	STEM PERFORMANCE					
Gaseous Fi	low from fan operation)		ACFM			
Gaseous F.	low ted from pitot traver	se)	ACFM			
Gaseous F. (implied	low from process operati	on)	ACFM			
Liquor Flo	ow		gpm			
Bypass (% of total gas flow)						
Throat Velocity						
	al Velocity (design)					
		e)				
Visible En	missions (residual) _					
ADDITIONAL	COMMENTS					
						
	Sheets Included	: A B	C			
		D E				
		G H				
Inspector's Signature						
Date Prepared						
	Reviewer's Signature					
	Date Reviewed					
	Date Filed					

LOCAT	ION	DATA SHEET NO.								
DESIG	NATION									
	т	-								
CLAIM	ED DENTIAL Yes No	•								
A. <u>D</u>	ESCRIPTIVE INFORMATION		•							
I	Mechanical Collector Type									
	CycloneS	ettling Chamber								
	Cyclone Bank D	ouble Vortex Cyclone	_							
	MulticloneO	ther (describe)	_							
1	Manufacturer		_							
	Model Number									
1	Date Installed									
	Process/Source Controlled									
. 1	Particulate Characteristics									
-										
B. <u>C</u>	OMPONENT INFORMATION									
	l. Cyclone									
	Diameter of Body		ft.							
	Material of Construc	tion								
•	Gauge of Metal									
		· · · · · · · · · · · · · · · · · · ·								
- :	2. Hoppers									
	Number									
	Slope									
	Insulation: Yes	No								
	Heating: Yes									
	Vibrators: Yes									

	Inspection No
	Data Sheet No.
	Preparer
	Confidential: Yes
	·
COME	PONENT INFORMATION (continued)
3.	Solids Removal (Check applicable items and providimensions)
	Rotary Valves
	Flapper Valves
	Screw Conveyors
	Pneumatic Conveyors
	Free Fall
4.	Fan/Motor
	Fan Manufacturer
	Model Number
	Blade Type: Radial Backward Forward
	Drive: Direct Belt
	Motor Manufacturer
	Model Number
	Rated Horsepower
	RPM '

C. SYSTEM LAYOUT



		Data Sheet No.	
		Preparer	
		Confidential: Yes	No
D.	EXTERNAL INSPECTION		
	Fan Inlet Static Pressure		in. of H ₂ O
	Fan Outlet Static Pressure _		
•.	Fan Motor Current		
	Fan Rotational Speed		_ rpm
	Fan Damper Position		a .
	Gas Temperature at Fan Inlet		_ °F
	Fan Vibration (low, moderate,	severe)	·
	Static Pressure at Collector		
	Static Pressure at Collector	Inlet	in. of H_2^- 0
	On-site Differential Pressure	Gauge Reading	
	Gas Temperature at Collector	Inlet	o _F
	Rotary Valve Rotational Speed	1	rpm
	Flapper Gate Frequency		_ (#/hr)
	Hopper Conditions (Check if a	applicable)	
	Cold		
	Dented		
	Warped		
	Corroded		

	Data Shoot No
	Data Sheet No.
	Preparer
	Confidential: Yes
NTERNAL INSPECTION	
Hoppers (plugged or corroded))
Hopper Baffles Nonexistent (Csion)	
Inlet Vanes Plugged/Eroded (0	
Cones Plugged (location, numb	oer)
Flow Disturbances (Characteri	ize severity)
·	
Outlet Tube Erosion (Characte	erize potential bypass
Correction (Characterists)	
Corrosion (Characterize)	
Scaling (Characterize)	

	1.	ispect	TOU NO	᠈.		
	Da	ata Sh	eet No	٠.		
	P:	repare	er			
	Ce	onfide	ential	: :	Yes_	No_
CONTROL SYSTEM PERFORM	RMANCE					
Air Flow Rate (impl:	ied from fan	opera	tion)			
Air Flow Rate (calcu	lated from	pitot	tube)			
Air Flow Rate (impl:	ied from pro	cess c	perat:	ion)	
Inlet Velocity						
Opacity						
	Sheets Incl					
	pueers inci-	aueu.	E			
			£	г —		
	Inspector's	Signa	ture .			
	Date Prepare	ed				
	Reviewer's					
	Date Review					

SOURCE NAME				SOURCE ID NUMBER OBSERVATION DATE										
ADDRESS					OBSERVER'S NAME (PRINT)									
				ORGANIZATION										
STATE	ZIP	PHONE		T	CERTIFIED BY									
					\\\-\-\-\-\-\-\-\-\-\-\-\-\-\-\-\-\-\-	L								
				SUN SHA	70'	NE						ATE		/.
PROCESS OPERATING MODE			STAR	MIT TIM	-	20	45	STOP	TIME	15	20	45		
CONTROL EQUIPMENT OPERATING MODE			IODE	1	0	15	30	45	31	0	15	30		
	••••••			•••••••••••••••••••••••••••••••••••••••	2					32				
	MISSION POINT		*******************************	• • • • • • • • • • • • • • • • • • • •	3 4					33				
	DINT HEIGHT	EMI	SSION POINT HEIC	SHT	5					35				·
ABOVE GRO	0110 55456	1	ATIVE TO OBSER	VEN	6					36				
DISTANCE T			ECTION TO SSION POINT		7 8					37		ļ		
					9					39				
DESCRIBE E					10					40				
***************************************	••••••	*********************	***************************************		11					41				
COLOR OF E	MISSIONS	CON	TINUOUS F	UGITIVE	13					43				
		INT	ERMITTENT		14					44				
WATER VAP	ORPRESENT	IF Y	ES, IS PLUME		16	· · ·				46				
140	YES 🔲	ATT		ETACHED	17					47				
AT WHAT PO	INT WAS OPACE	TY DETERMIN	IED		18					48				
		***************************************			20					50				
Descoure n	ACKCOOLIND				21					51				
DESCRIBE B.	ACKGROUND				22	-				52 53				
COLOR OF B	ACKGROUND	SKY	CONDITIONS		24					54				
WIND SPEED		WIN	ID DIRECTION		25 26					55 56			<u> </u>	
-	·		······		27					57				
AMBIENT TE	MPERATURE	REL	ATIVE HUMIDITY	r	28					58				
**MENTS					29 30					59 60				
		***************************************			AVERAGE OPACITY NUMBER OF READINGS						NGS AB	OVE		
*****************		•••••												
*******************	•••••		***************************************		RANGI	E OF C	PACITY					,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,		
SOURCE LA	VOUT CYETCH				READI	NGS			FROM_		то.			
SOURCE LAYOUT SKETCH											C	DRAW N	ORTH A	ARROV
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OBSERVER'S	SSIGNATURE		DATE	//	I HAVE RECEIVED A COPY OF THESE OPACITY OBSERVATIONS.									
VERIFIED B	y	<u> </u>	<u></u>		TITL	E	· c						ATE	/ /
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