



Research and Development

ENVIRONMENTAL ASSESSMENT OF AN
ENHANCED OIL RECOVERY STEAM
GENERATOR EQUIPPED WITH AN EPA
HEAVY OIL LOW-NO_x BURNER
Volume II. Data Supplement

Prepared for

Office of Air Quality Planning and Standards

Prepared by

Air and Energy Engineering Research
Laboratory
Research Triangle Park NC 27711

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ENVIRONMENTAL ASSESSMENT OF AN
ENHANCED OIL RECOVERY STEAM GENERATOR
EQUIPPED WITH AN EPA HEAVY OIL LOW-NO_x BURNER

Volume II
Data Supplement

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For

U.S. ENVIRONMENTAL PROTECTION AGENCY
Office of Research and Development
Washington, DC 20460

ABSTRACT

Comprehensive emission measurements and 30-day flue gas monitoring were performed on a 16-MW (55 million Btu/hr) enhanced oil recovery steam generator equipped with the EPA low-NO_x burner firing high-nitrogen crude. The 1-day comprehensive measurements included quantification of semivolatile organics and 73 trace elements; volatile organic sampling train (VOST) quantitation of volatile organic priority pollutants; EPA Method 5/8 for particulate and SO_x; controlled condensation for SO_x; Andersen impactors for particle size distribution; grab samples for N₂O; and continuous flue gas monitoring. NO_x emissions during the comprehensive tests averaged 70 ppm at 3 percent O₂, well below the target level of 85 ppm. CO emissions were below 30 ppm, and SO₂ averaged about 550 ppm. Solid particulates were emitted at about 27 ng/J (96 mg/dscm); condensible particulates were about half that level. Volatile organics (benzene, toluene, and ethylbenzene) were measured in the 0.4 to 20 ppb range. Semivolatile organics (naphthalene and phenol) were detected in the 0.3 ppb range. Subsequent continuous monitoring of flue gas criteria emissions showed NO_x below 80 ppm at 3 percent O₂ with an average of 70 ppm. CO emissions were generally less than 30 ppm.

CONTENTS

1	Introduction	1-1
2	Preliminary Tests and Equipment Calibration	2-1
3	Steam Generator Operating Data	3-1
4	Sampling Data Sheets	4-1
	4.1 Continuous Monitoring Data	4-2
	4.2 Field Data Sheets for EPA Method 5/8, SASS, VOST, Andersen Impactor, Controlled Condensation (CCS), and EPA Method 7	4-65
5	Analytical Results	5-1
	5.1 Fuel Proximate and Ultimate Analyses	5-2
	5.2 Particulate and Sulfur Oxides Emissions from Method 5/8 Samples	5-4
	5.3 Particulate Emissions from SASS Samples	5-12
	5.4 Particulate Emissions Size Distributions from Andersen Samples	5-17
	5.5 Sulfur Oxides Emissions from Controlled Condensation System Samples	5-26
	5.6 Trace Element Analyses of Fuel and SASS Samples	5-30
	5.7 Organic Analyses of SASS Samples: Total Chromatographable Organics (TCO), Gravimetric Organics (GRAV), Gas Chromatography Mass Spectrometry (GC/MS), and Infrared (IR) Spectra of Total Sample Extracts	5-44
	5.8 Volatile Organics Analyses of VOST Traps	5-53
	5.9 N ₂ O Emissions by GC/ECD	5-59
	5.10 NO _x Emissions by EPA Method 7	5-61

SECTION 1

INTRODUCTION

The purpose of this data supplement is to document test data in greater detail than was possible in Volume I (Technical Results) of this report. It is intended to provide sufficient detail for researchers to perform their own analysis of the data obtained. Readers are referred to the technical volume (Volume I) for objectives, description of the source tested, data interpretations, and conclusions.

The remaining sections of this data supplement contain the following information:

- Section 2: Preliminary Tests and Equipment Calibration -- Stack velocity traverse and nozzle sizing and flow calculations; equipment calibration data
- Section 3: Steam Generator Operating Data -- Field data sheets of steamer operating conditions from available test meters
- Section 4: Sampling Data Sheets -- Emission data obtained with continuous monitoring instrumentation. Operating data tables for combined EPA Methods 5/8 (for particulate mass and SO_x emissions), source assessment sampling system (SASS) (for trace element and organic emissions), volatile organic sampling train (VOST) (for volatile organic species emissions), Andersen impactor (for particulate size

distribution), controlled condensation system (for SO₂, SO₃), and EPA Method 7 (for NO_x certification)

Section 5: Analytical Results -- Fuel proximate and ultimate analyses; laboratory reports for particulate emissions and size distribution by gravimetric analyses; sulfur oxides emissions by wet chemical analysis; trace element analyses by spark source mass spectrometry (SSMS); atomic absorption spectroscopy (AAS) and other methods; total chromatographable organic (TCO) and gravimetric organic (GRAV) results, determination of organic compounds by gas chromatography/mass spectrometry (GC/MS) and infrared (IR) spectra of GRAV residues, volatile organics analyses of VOST traps by GC/MS; N₂O analysis by GC/electron capture detector (ECD); and laboratory analyses for NO_x by EPA Method 7.

SECTION 2
PRELIMINARY TESTS AND EQUIPMENT CALIBRATION

PRELIMINARY VELOCITY TRAVERSE

PLANT _____
DATE _____
LOCATION _____
STACK I.D. _____
BAROMETRIC PRESSURE, in. Hg _____
STACK GAUGE PRESSURE, in. H₂O _____
OPERATORS _____

SCHEMATIC OF TRAVERSE POINT LAYOUT

TRAVERSE POINT NUMBER	VELOCITY HEAD (Δp_s) , in. H ₂ O	STACK TEMPERATURE (T _s), °F
1	.27	
2	.35	
3	.37	415
4	.37	418
5	.38	429
6	.40	432
7	.42	435
8	.47	437
9	.47	438
10	.48	438
11	.50	438
12	.48	438
AVERAGE		

TRAVERSE POINT NUMBER	VELOCITY HEAD (Δp_s), in. H ₂ O	STACK TEMPERATURE (T_s), °F
1	0.20	
2	0.25	
3	0.23	417
4	0.23	417
5	0.23	417
6	0.23	417/43
7	0.23	417/43
8	0.23	417/43
9	0.23	417/43
10	0.23	417/43
11	0.23	417/43
12	0.23	417/43
13	0.23	417/43
14	0.23	417/43
15	0.23	417/43
16	0.23	417/43
17	0.23	417/43
18	0.23	417/43
19	0.23	417/43
20	0.23	417/43
21	0.23	417/43
22	0.23	417/43
23	0.23	417/43
24	0.23	417/43
25	0.23	417/43
26	0.23	417/43
27	0.23	417/43
28	0.23	417/43
29	0.23	417/43
30	0.23	417/43
31	0.23	417/43
32	0.23	417/43
33	0.23	417/43
34	0.23	417/43
35	0.23	417/43
36	0.23	417/43
37	0.23	417/43
38	0.23	417/43
39	0.23	417/43
40	0.23	417/43
41	0.23	417/43
42	0.23	417/43
43	0.23	417/43
44	0.23	417/43
45	0.23	417/43
46	0.23	417/43
47	0.23	417/43
48	0.23	417/43
49	0.23	417/43
50	0.23	417/43
51	0.23	417/43
52	0.23	417/43
53	0.23	417/43
54	0.23	417/43
55	0.23	417/43
56	0.23	417/43
57	0.23	417/43
58	0.23	417/43
59	0.23	417/43
60	0.23	417/43
61	0.23	417/43
62	0.23	417/43
63	0.23	417/43
64	0.23	417/43
65	0.23	417/43
66	0.23	417/43
67	0.23	417/43
68	0.23	417/43
69	0.23	417/43
70	0.23	417/43
71	0.23	417/43
72	0.23	417/43
73	0.23	417/43
74	0.23	417/43
75	0.23	417/43
76	0.23	417/43
77	0.23	417/43
78	0.23	417/43
79	0.23	417/43
80	0.23	417/43
81	0.23	417/43
82	0.23	417/43
83	0.23	417/43
84	0.23	417/43
85	0.23	417/43
86	0.23	417/43
87	0.23	417/43
88	0.23	417/43
89	0.23	417/43
90	0.23	417/43
91	0.23	417/43
92	0.23	417/43
93	0.23	417/43
94	0.23	417/43
95	0.23	417/43
96	0.23	417/43
97	0.23	417/43
98	0.23	417/43
99	0.23	417/43
100	0.23	417/43
AVERAGE		

ISOKINETIC SAMPLING WORKSHEET

Plant

Performed by

Date 2-1-83

Sample Location

Test No./Type 2057

$$K = \frac{782.687 (C_p)^2 (1-B_{wo})^2 P_s M_d}{K_o^2 M_s P_m}$$

where: K = Contant of fixed and assumed parameters (dimensionless)

Pitot coefficient (dimensionless)	C_p	1.00
Water vapor in the gas stream (proportion by volume)	B_{wo}	0.11
Absolute stack gas pressure (in. Hg)	P_s	29.51
Molecular weight, stack gas dry (lb/lb-mole)	M_d	30.36
Orifice coefficient (dimensionless)	K_o	0.62
Molecular weight, stack gas wet (lb/lb-mole) $M_d(1-B_{wo}) + 18(B_{wo})$	M_s	29.00
Absolute meter pressure (in. Hg)	P_m	29.38
$\frac{782.687 (\frac{0.72}{0.322})^2 (1-\frac{0.001}{27.00})^2 (\frac{29.51}{29.38}) (\frac{30.36}{29.00})}{(\frac{0.322}{27.00})^2 (\frac{27.00}{29.38}) (\frac{29.38}{29.51})}$	K	735.00

$$u \cdot y = 7.520$$

ISOKINETIC SAMPLING WORKSHEET

Plant CHENON

Performed by KEVIN HAN

Date 2/1/84

Sample Location _____

Test No./Type GASS

$$K = \frac{782.687 (C_p)^2 (1-B_{wo})^2 P_s M_d}{K_o^2 M_s P_m}$$

where: K = Contant of fixed and assumed parameters (dimensionless)

Pitot coefficient (dimensionless)	C _p	.816
Water vapor in the gas stream (proportion by volume)	B _{wo}	0.11
Absolute stack gas pressure (in. Hg)	P _s	Static -.5
Molecular weight, stack gas dry (lb/lb-mole)	M _d	CO ₂ 14 O ₂ - 3 N ₂ - 28
Orifice coefficient (dimensionless)	K _o	3.356 x .039
Molecular weight, stack gas wet (lb/lb-mole) M _d (1-B _{wo}) + 18(B _{wo})	M _s	
Absolute meter pressure (in. Hg)	P _m	29.26
$\frac{782.687 (\quad)^2 (1- \quad)^2 (\quad) (\quad)}{(\quad)^2 (\quad) (\quad)}$	K	38.419

NA / 3.69

ISOKINETIC NOZZLE CALCULATION
AND
SAMPLING RATE CALCULATION

Plant CORCORAN

Performed by KONTAKOS

Date 2/1/84

Sample Location _____

Test No./Type SPSS #1

$$N_d = \left(\frac{\Delta H T_s}{K T_m \Delta P} \right)^{.25}$$

where: N_d = Nozzle diameter (inches)

Average pressure differential across the orifice meter (in. H ₂ O)	ΔH	
Temperature stack gas, average (°F)	T_s	
Temperature of gas meter, average (°F)	T_m	
Stack gas velocity pressure (in H ₂ O)	ΔP	
$\left(\frac{(\quad)(\quad + 460)}{(\quad)(\quad + 460)(\quad)} \right)^{.25}$	N_d	

$$\Delta H = K (N_d)^4 \frac{T_m}{T_s} (\Delta P)$$

where: ΔH = Pressure differential across the orifice meter (in H₂O)

Nozzle diameter, actual (inches)	N_d	.674
Temperature of gas meter (°F)	T_m	
Temperature of stack gas (°F)	T_s	
Stack gas velocity pressure (in H ₂ O)	ΔP	
$\left((\quad)(\quad)^4 \frac{(\quad + 460)}{(\quad + 460)} (\quad) \right)$	ΔH	
Magic number _____ () ⁴	$K(N_d)^4$	7.93

ANDERSEN SAMPLING CALCULATIONS

Plant Chamon SVS-69
 Date 2-22-84
 Test Location Outlet
 Pitot Coefficient (C_p) _____
 Duct Dimension _____

Barometric Pressure (P_G) _____ " Hg
 Static Pressure (P_{st}) _____ " H₂O
 Meter Temp (T_m) _____ °F
 Meter Rate (R_m) _____ cfm
 Clock Time _____

1) Stack Pressure: $P_s = P_b + \frac{P_{st}}{13.6} = \underline{29.36} + \frac{\quad}{13.6} = \underline{29.36}$ in. Hg.

2) Mole Fraction Dry Gas: $M_f = 1 - \frac{\%H_2O}{100} = 1 - \frac{11}{100} = \underline{.89}$

3) Mol. Wt. Dry Flue Gas:

$$MW_d = (0.44 \times \%CO_2) + (0.32 \times \%O_2) + (0.28 \times \%CO) + (0.28 \times \%N_2) - (0.44 \times \underline{14.0}) + (0.32 \times \underline{2.5}) + (0.28 \times \quad) + (0.28 \times \underline{83.5}) = \underline{30.34}$$

4) Mol. Wt. Flue Gas:

$$MW_s = (MW_d) \times (M_f) + [18 \times (1 - M_f)] = \underline{32.34} \times \underline{.89} + [18 \times (1 - \underline{.11})] = \underline{28.98}$$

5) Stack Gas Velocity:

$$V_s = 85.49 \times (C_p) \times \sqrt{\Delta P_{avg}} \times \sqrt{\frac{T_s + 460}{P_s \times MW_s}} = 85.49 \times \underline{.82} \times \sqrt{\underline{.44}} \times \sqrt{\frac{\underline{530} + 460}{\underline{29.36} \times \underline{28.98}}} = \underline{50.16} \text{ fps}$$

6) Sample Rate:

$$Q_n = 0.327 \times (V_s) \times (D_n)^2 = 0.327 \times \underline{50.14} \times (\underline{.25})^2 = \underline{1.02} \text{ acfm}$$

7) Meter Rate:

$$R_m = (Q_n) \times \frac{P_s}{P_m} \times \frac{T_m + 460}{T_{st} + 460} \times M_f \times \alpha = \underline{1.025} \times \frac{\underline{29.36}}{\underline{29.39}} \times \frac{\underline{70} + 460}{\underline{530} + 460} \times \underline{.89} = \underline{0.488} \text{ cfm}$$

$$1.68 \left(\frac{R_m}{K_o} \right)^2 = \Delta H \quad 1.68 \left(\frac{\quad}{\underline{.67}} \right)^2 = \underline{0.89} \text{ "H}_2\text{O}$$

CONTROL MODULE CALIBRATION

Module I.D. #105
Date 10-5-83

Barometric Pressure (in. Hg) 30.07
Primary Meter I.D. 433583

Ambient Temperature (°F) 78°
Operator S.A. Smith

Orifice Size	Orifice Reading ΔH (in H ₂ O)	Primary Meter Gas Volume V_p (ft ³)	Meter Box Gas Volume V_d (ft ³)	Temperature						Time θ (min)	Meter Correction Factor α	Orifice Coefficient K_o				
				Primary Meter			Meter Box Meter									
				Inlet T_{pi} (°F)	Outlet T_{po} (°F)	Average T_p (°F)	Inlet T_{di} (°F)	Outlet T_{do} (°F)	Average T_d (°F)							
Small Orifice 0.187	.6	23.710	22.960	98	78	93	77	86.5	69	72	68	71	70	58.5	1.000	.670
	2.0	22.595	22.145	78	79	77	76	77.5	72	74	71	72	72.3	30.2	.994	.677
	4.0	26.155	25.680	79	84	76	78	79.3	74	74	72	73	73.3	25.7	1.003	.650
	5.4	21.655	21.230	84	86	78	79	81.8	74	75	73	74	74	18.2	1.008	.654
Medium Orifice 0.281	.6	70.235	68.985	86	86	79	81	83	75	76	74	76	75.3	65.3	.998	1.771
	2.0	43.130	42.265	86	99	81	85	87.8	76	80	76	77	77.3	23.0	1.004	1.688
	4.0	30.820	30.175	99	105	85	89	94.5	80	80	77	77	78.5	12.1	1.018	1.620
	5.4	33.060	32.340	105	109	89	92	98.8	80	83	77	78	79.5	11.2	1.027	1.614
Large Orifice 0.358	.6	37.865	36.910	109	104	92	90	98.8	83	81	78	79	80.3	16.9	1.010	3.672
	2.0	33.680	33.210	104	114	90	94	100.5	81	85	79	80	81.8	8.9	1.025	3.392
	4.0	73.560	73.500	114	121	94	103	108	85	90	80	82	84.3	14.4	1.053	3.231
	5.4	25.950	26.155	121	122	103	105	112.8	90	92	82	84	87	4.5	1.069	3.131

$$\alpha = \frac{V_d (P_B + \frac{\Delta H}{13.6}) (T_p + 460)}{V_p (P_B) (T_d + 460)}$$

$$K_o = \frac{V_p}{0.05 \sqrt{\frac{\Delta H (T_d + 460)}{P_B (28.96)}}}$$

Orifice	Avg. α	Avg. K_o
Small	1.001	.662
Medium	1.012	1.673
Large	1.039	3.356

SECTION 3
STEAM GENERATOR OPERATING DATA

Time	Lat	Long	Alt	Dist	Time	Lat	Long	Alt	Dist
9.30		264	3.6	2516.1	1000	535	4.70	1.84	65
9.45	33312.1	265	3.6	2548.0	1000	535	4.80	2.00	65
10.00	33314.10	265	3.6	2581.7	1000	535	4.65	3.10	65
10.15	33316.45	266	3.6	2618.5	1000	535	4.50	2.40	67
10.30	33318.50	267	3.6	2654.1	1000	535	4.52	2.40	67
10.45	33320.26	267	3.6	2693.5	1020	535	4.41	2.58	66
11.00	33323.18	267	3.6	2729.5	1020	535	4.70	2.56	66
11.15	33325.49	267	3.6	2767.0	1020	535	4.68	2.11	66
11.30	33327.37	264	3.6	2800.2	1020	535	4.73	2.22	69
11.45	33329.53	265	3.6	2836.4	1020	535	4.82	2.30	70
12.00	33331.85	268	3.6	2874.2	1020	535	4.72	2.28	68
12.15	33334.30	267	3.6	2912.8	1020	535	4.65	2.32	67
12.30	33336.28	267	3.6	2946.0	1020	535	4.60	2.33	68
12.45	33338.54	267	3.6	2984.6	1020	535	4.65	2.24	67
13.00	33341.05	266	3.6	3024.3	1020	535	4.56	2.43	72
13.15	33342.91	267	3.6	3057.4	1020	535	4.60	2.36	70
13.30	33345.01	265	3.4	3095.2	1010	538	4.71	2.06	67
13.45	33347.40	266	3.4	0293	1010	535	4.70	2.03	73
14.00	33349.27	264	3.4	0599	1020	535	4.70	2.01	71
14.15	33351.69	266	3.4	0962	1080	545	4.76	1.97	71
14.30	33354.57	266	3.4	1429	1190	560	4.65	2.19	71
14.45	33356.00	266	3.4	165.2	1220	560+	4.62	2.48	73
15.00	33357.80	268	3.4	201.8	1240	560+	4.65	2.40	70
15.15	33360.25	267	3.4	238.6	1250	560+	4.62	2.40	73
15.30	33362.53	267	3.4	268.1	1280	560+	4.63	2.33	72
15.45	33364.61	269	3.4	299.3	1280	560+	4.71	2.34	70
16.00	33367.07	-	3.4	336.7	1280	570+	4.70	2.35	68
16.18	33369.78	-	3.4	377.7	1290	570+	4.70	2.35	68
16.30	33371.48	-	3.4	404.0	1300	570+	4.76	2.45	69
16.45	33373.75	-	3.4	439.0	1300	570+	4.70	2.30	55
17.00	33376.26	269	3.4	475.9	1300	560+	4.70	2.30	69
17.15	33378.42	267	3.4	511.7	1300	560+	4.55	2.29	70
17.30	33380.28	268	3.4	540.8	1300	560+	4.70	2.32	67
17.45	33382.40	269	3.4	574.6	1300	560+	4.67	2.35	69

STEAMER OPERATING DATA (COMPREHENSIVE TEST - 2-1-84)

Time	Oil Flow		Feedwater		Steam		Combustion Air		
	Total Gallons	Temperature (°F)	BPD X 1000	Total Barrels	Pressure (PSI)	Temperature (°F)	Primary Air Flow - a mv	Secondary Air Flow - b mv	Temperature At Fans (°F)
1800	33384.93	269	3.4	606.9	1300	560 ⁺	4.74	2.30	?
1815	33386.53	269	3.4	643.4	1300	560 ⁺	4.70	2.26	69
1830	33389.24	269	3.4	678.0	1300	560 ⁺	4.70	2.33	70
1845	-	269	3.4	710.4	1300	560 ⁺	4.70	2.36	69
1900	-	269	3.4	745.7	1300	560 ⁺	4.54	2.79	69
1920	-	270	3.4	794.0	1300	560 ⁺	4.68	2.43	68
1945	334006.0	268	3.4	850.5	1320	560 ⁺	4.60	2.65	67
2000	334029.0	268	3.4	885.4	1320	560 ⁺	4.41	2.78	66
2015	334048.0	267	3.4	917.3	1320	560 ⁺	4.26	3.00	65
2030	334075.1	267	3.35	953.8	1320	560 ⁺	4.40	2.30	64
2045	334094.4	267	3.35	982.2	1320	560 ⁺	4.38	2.73	63
2100	334120.2	267	3.35	1021.6	1330	560 ⁺	4.46	2.92	63
2115	334143.8	266	3.3	1055.9	1330	560 ⁺	4.39	2.90	61
2145	334188.0	267	3.3	1123.5	1320	560 ⁺	4.74	2.21	61
a	Primary	Air Flow	(scfm)	=	63777	$\left(\frac{V}{T(R)}\right)^{1/2}$			
b	Secondary	Air Flow	(scfm)	=	82777	$\left(\frac{V}{T(R)}\right)^{1/2}$			

SECTION 4
SAMPLING DATA SHEETS

- 4.1 Continuous Monitoring Data
- 4.2 Field Data Sheets for EPA Method 5/8, SASS, VOST, Andersen Impactor, Controlled Condensation (CCS), and EPA Method 7

4.1 CONTINUOUS MONITORING DATA

ACUREX
Aerotherm

Ambient Temperature 54.0 F
Barometric Pressure 29.44 (11.1)
Static Pressure Duct _____
Fuel 150000 150000

4
t
(w)

ACUREX
Aerotherm

Ambient Temperature 57°F 43°F
Barometric Pressure 29.97 (29.29) 29.97 (29.9)
Static Pressure Duct _____
Fuel 200LBS 100LBS

4-4

ACUREX
Aerotherm

Ambient Temperature _____
Barometric Pressure 29.54 (in Hg)
Static Pressure Duct _____
Fuel 1.545 2.405

[illegible]

FIELD DATA SHEET



Plant CHEVRON (KER)
 Location SUS 27-69
 Operator Basz
 Date 1-24-84
 Load Range _____

Ambient Temperature 52°F 72°F
 Barometric Pressure 29.65 (100) 29.54 (14.5)
 Static Pressure Duct _____
 Fuel Jet-A

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H2O %	Stack Gas Temp °F	COMMENTS
				O2 %	CO2 %	CO ppm	SO2 ppm	NO ppm	NOx ppm	NO2 ppm	NO ppm	NOx ppm	NO2 ppm	Total HC	Methane	Non-Methane HC			
0030				3.6		15	560		71										
0130				3.4		15	572		69										
0230				3.5		15	580		67										
0330				3.5		15	571		70										
0430				3.5		20	576		62										
0530				3.6		15	561		65										
0630				3.5		15	569		71										
0730				3.2		25	570		67										
0830				3.3		10	586		67										
0930				3.2		15	552		69										
1030				3.6		10	560		65										
1130				2.1		10	577		63										
1230				3.3		5	528		62										
1308				3.1		5	532		60										
1423				3.2		5	523		60										
1438				3.3		5	515		59										
1453				3.2		5	511		59										
1503				3.0		5	524		59										
1523				3.4		8	520		57										
1538				3.1		5	525		59										
1653				3.3		20	561		65										
1708				3.3		25	562		65										
1723				3.3		25	557		64										
1738				3.2		25	554		65										
1753				3.3		30	555		64										
1808				3.2		25	560		63										AVERAGE
1823				2.5		25	589		64										
1838				2.4		30	589		65										

Ambient Temperature _____

Barometric Pressure _____

Static Pressure Duct _____

Fuel _____

Fuel _____

[illegible]

ACUREX
Aerotherm

Ambient Temperature 61°F
Barometric Pressure 29.50 (1100)
Static Pressure Duct _____
Fuel 100% 100%

[illegible]

ACUREX
Aerotherm

Ambient Temperature 58°F

Barometric Pressure 29.54 (1200)

Static Pressure Duct _____

Fuel Leads Count

AVERAGE

FIELD DATA SHEET



Plant CHEVRON (EER)
 Location _____
 Operator BEST
 Date 1-27-84
 Load Range _____

Ambient Temperature _____
 Barometric Pressure _____
 Static Pressure Duct _____
 Fuel LOWESS CRACK

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
0205				3.0		5	626		15										
0235				2.9		5	630		12										
0305				2.9		5	637		17										
0335				3.0		5	658		15										
0355				2.8		10	638		16										
0425				2.9		0	650		16										
0435				3.1		5	634		12										
0455				3.0		5	612		15										
0505				3.0		5	621		14										
0535				3.2		10	621		18										
0555				2.9		10	623		18										
0605				2.8		5	617		17										
0635				3.1		10	623		11										
0655				3.3		10	621		29										
0705				3.2		10	622		33										
0735				2.9		10	621		11										
0805				2.9		12	611		10										
0847				2.7		15	573		70										
0849				2.6		15	612		19										
0904				2.7		10	612		71										
0917				2.7		15	602		17										
0934				2.7		16	590		19										
0949				2.8		20	622		18										
1004				2.9		20	550		16										
1019				2.8		25	543		16										
1034				2.7		25	577		14										
1049				2.8		25	508		13										
1104				2.7		26	575		10										
AVERAGE																			

4-10

ACUREX
Aerotherm

Ambient Temperature _____

Barometric Pressure _____

Static Pressure Duct _____

Fuel _____

Fuel _____

4-11

FIELD DATA SHEET



Plant CHEVRON (GER)
 Location 8V5-67
 Operator BEST
 Date 1-28-84
 Load Range _____

Ambient Temperature 67°F 56°F
 Barometric Pressure 29.42 (29.5) 29.32 (29.5)
 Static Pressure Duct _____
 Fuel 1.6405 (2.00)

4-12

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
1204				2.7		25	584		75										
1219				2.7		25	574		75										
1234				2.8		25	557		78										
1249				2.9		20	553		77										
1304				2.9		20	556		77										
1319				2.9		15	567		77										
1334				2.9		10	567		76										
1349				2.9		15	566		76										
1404				2.8		15	567		77										
1419				2.8		15	569		74										
1434				2.8		20	576		74										
1449				2.7		20	581		78										
1504				2.7		15	573		79										
1519				2.9		10	581		77										
1534				3.0		15	528		73										
1549				2.9		10	579		81										
1604				2.8		10	583		79										
1619				2.8		10	585		78										
1634				2.7		10	587		78										
1649				3.0		5	598		77										
1707				2.9		10	593		82										
1719				2.8		20	595		79										
1734				2.9		20	587		80										
1749				2.9		20	583		81										
1804				2.9		20	575		83										
1819				2.9		15	594		84										
1834				2.6		10	585		83										
1849				3.0		10	513		76										
AVERAGE																			

ACUREX
Aerotherm

Ambient Temperature _____

Barometric Pressure _____

Static Pressure Duct _____

Fuel _____

Fuel _____

4-13

FIELD DATA SHEET



Plant HEURON (EGR)
 Location SVS-69
 Operator BEST
 Date 1-29-84
 Load Range _____

Ambient Temperature 54°F
 Barometric Pressure 29.32 (102.1) 29.18 (100.1)
 Static Pressure Duct _____
 Fuel 1.5005 4.000

4-14

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED						CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC		
0004				2.9		30	570		76									
0019				3.0		30	565		73									
0034				2.9		30	576		70									
0049				2.9		30	581		75									
0101				2.9		30	589		75									
0117				2.9		36	587		72									
0134				2.8		35	589		70									
0149				2.9		35	586		72									
0204				2.7		40	597		71									
0219				2.8		35	588		72									
0234				2.9		35	591		71									
0249				3.0		35	598		72									
0304				2.8		35	616		70									
0319				2.5		35	610		70									
0334				3.7		40	598		71									
0349				2.8		40	595		71									
0404				2.9		40	595		70									
0419				2.8		40	591		73									
0434				2.5		40	600		71									
0449				2.9		40	594		74									
0504				2.8		45	577		76									
0519				2.8		40	580		72									
0534				2.8		40	573		71									
0549				2.8		40	570		68									
0604				2.8		40	578		65									
0619				2.7		40	589		64									AVERAGE
0634				2.8		40	586		67									
0649				3.0		40	587		67									

ACUREX
Aerotherm

Load Range_____

[illegible]

FIELD DATA SHEET



Plant CHEVRON E&E
 Location SUS - 69
 Operator BEST
 Date 1-30-84
 Load Range _____

Ambient Temperature 58°F
 Barometric Pressure 29.43 (0200) 29.30 (1650)
 Static Pressure Duct _____
 Fuel LEPSE CRUDE

4-16

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
0000																			initial run
0015				3.0	12.5	8	550		61										strip charts
0030				2.9	12.5	8	555		61										
0045					12.5	5	560												
0100					12.5	8	535												
0115						8	570												
0130						10	575												
0145						12	580												
0200						10	560												
0215						10	565												
0230						10	565												
0245						10	575												
0300						10	585												
0315						10	590												
0330						13	590												
0345						13	570												
0400						13	580												
0415						13	565												
0430						13	560												
0445						13	555												
0500						13	550												
0515						13	550												
0530						15	555												
0545						15	550												
0600						15													
																			AVERAGE

FIELD DATA SHEET



Plant CHEVRON (FER)
 Location SUS-69
 Operator BEST
 Date 1-30-84 (CONTINUED)
 Load Range _____

Ambient Temperature _____
 Barometric Pressure _____
 Static Pressure Duct _____
 Fuel _____

4-17

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
0615						15													
0630				lost	lost	15	lost		lost										
0645				lost	lost	15	lost		lost										
0700				lost	lost	15	lost		lost										
0715				lost	lost	12	lost		lost										
0730				lost	lost	14	lost		lost										
0745						16													
0800						20													
0815						23													
0830						23													
0845						24													
0900						25													
0915						25													
0930				↓	↓	25	↓		↓										
				0.0	10.2	115	15		0										0930 ATTEMPT TO
				6.8	18.0	175	505		90										ZERO
					17.8		503		90										SEEN
																			SEEN GDS 14-16
																			LEAK CHECK OK
																			UNIT HAD PROBLEMS
																			RUNNING WITH
																			PROBLEMS - CONTROLS
																			DETERM. STATUS 1530
																			AVERAGE

FIELD DATA SHEET



Plant CHEVRON (EER)
 Location SUS -69
 Operator BEST
 Date 1-30-84 (CONTINUED)
 Load Range _____

Ambient Temperature _____
 Barometric Pressure _____
 Static Pressure Duct _____
 Fuel _____

4-18

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
1620	START			3.4	13.2	25	505		64										RECURRANT 1540
1630				3.5	13.2	25	505		65									1410	START TEST AT 1620
1645				3.7	13.2	25	505		65										
1700				3.7	13.2	25	500		65										CO VERY NOISEY
1715				3.7	13.2	25	500		63										
1730				3.7	13.3	25	500		62										
1745				3.7	13.4	25	500		62										
1800				3.7	13.3	25	505		62										
1815				3.6	13.3	25	510		62										
1830				3.6	13.4	25	510		63										
1845				3.7	13.5	25	515		64										
1900				3.7	13.6	25	515		66										
1915				3.7	13.5	25	520		67										
1930				3.7	13.4	25	520		67										
1945				3.7	13.4	25	520		68										
2000				3.7	13.4	25	520		67										
2015				3.6	13.4	25	520		70										
2030				3.5	13.4	25	520		70										
2045				3.6	13.4	25	520		67										
2100				3.6	13.4	25	520		62										
2115				3.5	13.4	25	520		67										
2130				3.5	13.4	25	520		68										
2145				3.7	13.4	25	523		68										
2200				3.6	13.4	25	523		68										
2215				3.6	13.4	25	524		65										
																			AVERAGE

ACUREX
Aerotherm

Ambient Temperature _____
Barometric Pressure _____
Static Pressure Duct _____
Fuel _____

[illegible]

ACUREX
Aerotherm

Ambient Temperature 66°F
Barometric Pressure 29.34 (1800)
Static Pressure Duct _____
Fuel Gasoline

[illegible]

FIELD DATA SHEET



Plant Cheson (EER)
 Location SVS-69
 Operator Best
 Date 1-31-89 (Cont)
 Load Range _____

Ambient Temperature _____
 Barometric Pressure _____
 Static Pressure Duct _____
 Fuel _____

4-21

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
1800	Start				14.3	15	573		72										3.60 gpm/gal
1815					14.0	15	573		72										unit not fixed until later afternoon
1830					14.0	15	573		72										
1845					13.8	15	573		72										
1900					13.5	15	573		71										Calibrated at 1740
1915					13.4	15	573		71										
1930					13.4	15	573		71										Disturbance last left on 2.00 gpm/gal
1945					13.3	15	575		73										
2000					13.2	15	580		74										
2015					13.2	15	580		74										3.00 gpm/gal between 2.4 & 3.00 gpm/gal
2030					13.2	15	580		74										
2045					13.2	15	580		73										
2100					13.2	15	580		75										
2115					13	15	580		76										
2130					13	15	580		75										
2145					13.1	15	580		77										
2200					13.1	15	580		71										
2215					13.1	15	585		72										
2230					13.1	15	590		73										
2245					13.1	15	590		74										
2300					13.1	15	590		70										
2315					13.1	15	590		69										
2330					13.1	15	590		69										
2345					13.1	15	590		71										
2360					13.1	15	593		71										
AVERAGE																			

FIELD DATA SHEET



Plant Choron (IEEP)
 Location SVS-69
 Operator Best
 Date 2-1-84
 Load Range _____

Ambient Temperature _____
 Barometric Pressure _____
 Static Pressure Duct _____
 Fuel Gas

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H2O %	Stack Gas Temp °F	COMMENTS
				O2 %	CO2 %	CO ppm	SO2 ppm	NO ppm	NOx ppm	NO2 ppm	NO ppm	NOx ppm	NO2 ppm	Total HC	Methane	Non-Methane HC			
0009				2.8	13.2	9	583		72										From duct at 10
0024				2.7	13.3	6	587		72										
0038				2.8	13.1	14	589		69										
0053				2.8	13.3	15	587		71										
0105				2.7	13.3	16	581		72										
0121				2.7	13.3	14	571		71										
0139				2.8	13.2	14	585		74										
0202				2.7	13.2	14	589		72										
0219				2.8	13.3	13	580		74										
0242				2.8	13.2	13	588		73										
0302				2.8	13.3	14	587		72										
0322				2.8	13.2	15	586		73										
0337				2.7	13.2	7	578		69										
0350				2.7	13.3	14	578		71										
0404				2.7	13.3	15	567		70										
0413				2.6	13.4	15	574		71										
0438				2.7	13.2	15	579		71										
0443				2.8	13.2	13	574		73										
0501				2.8	13.2	14	578		72										
0508				2.8	13.2	14	575		72										
0523				2.8	13.2	13	581		71										
0538				2.8	13.2	13	587		69										
0602				2.7	13.2	11	583		72										
0617				2.8	13.2	11	576		73										
0639				2.8	13.2	14	581		73										
0654				2.7	13.2	11	576		72										
0659				2.8	13.2	13	574		74										
0714				2.7	14.5	15	578		76										
AVERAGE																			

FIELD DATA SHEET



Plant Chow (FER)
 Location SVS-69
 Operator Best
 Date 2-1-84
 Load Range _____

Ambient Temperature _____
 Barometric Pressure _____
 Static Pressure Duct _____
 Fuel _____

4-23

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
0720																			calculated 0720
				0.0	0.0	-7	0		-1.5										interup
				7.35	18.3	18.2	553		9.2										zero
				7.1			553		9.0										skan
																			stronger
0759				2.7	14.3	25	594		68										
0814				2.9	14.1	24	555		70										
0828				3.0	13.8	25	551		69										
0843				3.5	13.1	20	531		71										
0901				2.4	13.5	43	564		80										
0914				2.5	13.1	25	574		75										
0928				2.5	12.7	24	572		77										
0945					13.7	28			74										
1000				2.2	13.2	23	594		71										
1015				2.9	13.7	23	566		70										
1038				3.3	14.0	23	591		67										
1053				2.7	13.5	21	571		70										
1108				2.7	12.8	24	567		70										
1122				2.6	12.6	26	569		71										11/28 1 SVS etc 1
1136				2.7	12.2	22	559		70										
1143				2.7	12.2	23	565		70										
1157				2.7	12.6	24	563		68										
1218				2.4	13.3	25	573		68										
1235				2.7	12.7	26	561		68										
1247				2.8	12.5	25	566		67										11/28 (AVERAGE 2.2)
1305				2.4	13.3	24	566		68										
1322				2.8	12.9	23	561		67										

ACUREX
Aerotherm

Ambient Temperature _____

Barometric Pressure _____

Static Pressure Duct _____

Fuel _____

4-24

ACUREX
Aerotherm

Ambient Temperature _____

Barometric Pressure _____

Static Pressure Duct _____

Fuel _____

4-25

FIELD DATA SHEET



Plant Choron (EEA)
 Location SVS-69 Outlet
 Operator Best
 Date 2-2-84
 Load Range _____

Ambient Temperature _____
 Barometric Pressure _____
 Static Pressure Duct _____
 Fuel Heavy crude

4-26

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
0010				2.6	12.8	23	578		75										all values from
0025				2.7	12.7	22	579		76									461	rotated 1/2
0040				2.7	12.7	25	583		77										
0055				2.7	12.6	23	586		78									461	
0110				2.7	12.6	23	586		*										
0125				2.7	12.6	23	578		82									466	
0140				2.5	12.6	24	572		80										
0155				2.6	12.5	23	590		80									468	
0210				2.7	12.5	23	598												
0225				2.7	12.5	24	597											468	
0240				2.7	12.5	21	601												
0255				2.8		22	604											467	
0310				2.7		23	602												
0325				2.7		27	601											467	
0340				2.7			590												
0355				2.7		23	579											467	
0410				2.7		24	590												
0425				2.7		24	591											468	
0440						23	585												
0455						23	588											469	
0510						25	593												
0525						23	591											468	
0540						22	601												
0555						22	573											471	
0610						22	574												
0625						23	574											467	
0640						24	596												
0655						22	588											468	
AVERAGE																			

FIELD DATA SHEET



Plant _____

Ambient Temperature _____

Location _____

Barometric Pressure _____

Operator _____

Static Pressure Duct _____

Date 2-2-84 (cont.)

Fuel _____

Load Range _____

4-27

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
0710						25	588												
0725						22	598											468	
0740						21	611												
0755						21	607											466	
0810						20	594												
0825						23	598											450	
0840						21	593												
0855				2.8	12.0	20	590		66									462	
																			0900 cal external
				0.0	0.0	46.5	10.5		0										zero
				7.25	17.9	18.5	545		87.5										zero
																			off on gas
																			replaced with
																			Knobbed okay
0940				2.5	13.9	20	612		84										
0955				2.6	13.7	24	589		85									467	
1010				2.5	13.6	20	587		84										
1025				2.4	13.8	23	579		84									464	
1040				2.6	13.4	21	579		86										
1055				2.6	13.6	21	574		85									467	
1110				2.6	13.2	23	579		84										
1125				2.4	13.4	20	586		77									477	
1140				2.7	13.4	20	585		72										
1155				2.5	13.2	23	583		69									492	
1210				2.8	12.1	19	573		67										
1225				2.4	12.9	21	581		67									497	
																			AVERAGE

FIELD DATA SHEET



Plant _____

Ambient Temperature _____

Location _____

Barometric Pressure _____

Operator _____

Static Pressure Duct _____

Date 2-2-84 (cont.)

Fuel _____

Load Range _____

4-28

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
1240				2.7	12.9	21	573		68										
1255				2.7	13.5	18	576		69									496	
1310				2.7	13.3	23	577		67										
1325				2.6	13.2	23	567		66									495	
1340				2.8	12.9	18	566		68										
1355				2.6	13.4	21	578		68									478	
1410				2.6	12.9	21	568		69										
1425				2.6	13.2	20	568		67									498	
1440				2.7	13.7	22	563		65										
1455				2.6	13.4	19	567		67									495	
1510				2.6	13.1	21	568		68										
1525				2.6	13.2	21	567		70									498	
1540				2.6	13.4	21	564		69										
1555				2.6	13.2	21	562		68									494	
																			1600 entered and
				0.0	-0.1	+7	+9		0										zero
				7.1	17.2	180	596		86.5										span
																			span gas
																			Water accumulating
																			in lower; left and
																			on ambient air brought
																			to dry lines
																			AVERAGE

FIELD DATA SHEET



Plant Choron EER
 Location SVS-69
 Operator Bent
 Date 2-3-84
 Load Range _____

Ambient Temperature 63°F
 Barometric Pressure (200) 29.32
 Static Pressure Duct _____
 Fuel Gasoline

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED						CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC		
0840	calibrate																	1320 Dump smoke gauge reading < 1401
0900	Start																	Opsi with probe blocked
0910				2.8	13.7	19	—		82								573	
0925				2.8	13.8	17	673		75									
0940				2.7	13.7	18	674		74								496	
0955				2.6	13.5	18	663		75									
1010				2.7	13.3	17	660		72								489	
1025				2.6	13.3	17	669		72									
1040				2.6	13.2	15	665		71								486	
1055				2.6	13.4	18	670		72									
1110				2.5	13.0	17	671		74								489	
1125				2.7	12.9	13	668		72									
1140				2.6	13.1	22	666		71								489	
1155				2.6	13.0	23	661		69									
1210				2.8	12.8	22	657		71								502	
1225				2.7	12.6	24	656		72									
1240				2.8	12.5	21	652		70								502	
1255				2.7	13.0	23	632		69									
1310				3.0	12.7	24	624		68								502	
1325				2.8	12.7	20	638		68									
1340				2.9	12.6	23	638		69									
1355				2.7	12.6	25	643		70									
1410				2.6	12.6	25	644		69									
1425				2.7	12.6	24	640		69									
																		AVERAGE

4-29

FIELD DATA SHEET



Plant _____

Location _____

Operator _____

Date 2-3-84

Load Range _____

Ambient Temperature _____

Barometric Pressure _____

Static Pressure Duct _____

Fuel _____

4-30

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
1440	internal cal			0.0	0.0	+5	+14		890										giso
				7.15	17.1	170	890		91.5										span
																			span gas
1655	recalibrate																		
1710	stack																		Stack T.C. out
1721				2.7	13.9	22	637		74										→ fixed SO ₂ analyzer
1736				2.8	13.9	20	614		74										
1751				2.8	13.8	23	601		73										
1806				2.7	13.7	23	597		74										
1821				2.7	13.5	23	594		74										
1836				2.8	13.4	22	589		73										
1851				2.8	13.4	22	587		70										
1906				2.8	13.5	20	587		69										
1921				2.8	13.5	20	587		69										
1936				2.7	13.6	19	574		68										
1951				2.7	13.6	23	568		69										
2006				2.7	13.6	26	545		71										
2021				2.7	13.6	26	545		71										
2036				2.7	13.6	32	544		71										
2051				2.8	13.6	30	545		70										
2106				2.8	13.6	29	543		71										
2121				2.7	13.7	34	543		68										
2136				2.8	13.7	35	543		68										
2151				2.8	13.6	32	541		66										
																			AVERAGE

ACUREX
Aerotherm

Ambient Temperature _____

Barometric Pressure _____

Static Pressure Duct _____

Fuel _____

Load Range _____

[illegible]

FIELD DATA SHEET



Plant Choron (EER)
 Location SVS-69
 Operator Best
 Date 2-4-84
 Load Range _____

Ambient Temperature _____
 Barometric Pressure _____
 Static Pressure Duct _____
 Fuel _____

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H2O %	Stack Gas Temp °F	COMMENTS
				O2 %	CO2 %	CO ppm	SO2 ppm	NO ppm	NOx ppm	NO2 ppm	NO ppm	NOx ppm	NO2 ppm	Total HC	Methane	Non-Methane HC			
0006				2.6	13.8	38	533		70										
0021				2.7	14.5	39	529		74										
0051				2.7	14.2	38	529		73										
0106				2.7	14.3	25	582		75										
0121				2.8	14.2	24	617		75										
0136				2.8	14.1	26	628		71										
0151				2.9	14.0	19	622		72										
0206				2.9	13.9	20	629		71										
0221				2.9	13.9	22	627		75										
0236				2.8	13.9	21	626		75										
0251				2.8	13.8	20	640		74										
0306				2.8	13.7	20	647		71										
0321				2.8	13.6	21	646		71										
0336				2.8	13.7	21	651		80										
0351				2.6	13.7	21	658		82										
0406				2.6	13.7	20	660		82										
0421				2.7	13.4	19	656		78										
0436				2.9	13.4	18	658		77										
0451				2.9	13.3	20	666		77										
0506				2.6	13.5	19	678		77										
0521				2.6	13.3	19	672		78										
0536				2.8	13.2	17	661		78										
0551				2.4	13.4	20	680		81										
0606				2.6	13.3	19	678		88										
0621				2.5	13.5	21	671		88										
AVERAGE																			

4-32

ACUREX
Aerotherm

Ambient Temperature _____

Barometric Pressure _____

Static Pressure Duct _____

Fuel _____

Load Range_____

[illegible]

FIELD DATA SHEET



Plant Chooon CEE R
 Location SVS-69
 Operator Best / Milburn
 Date 2-5-84
 Load Range _____

Ambient Temperature 69°F 58°F
 Barometric Pressure 29.34 (1435) 29.42 (2030)
 Static Pressure Duct _____
 Fuel lease crude

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED						CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H2O %	Stack Gas Temp °F	COMMENTS
				O2 %	CO2 %	CO ppm	SO2 ppm	NO ppm	NOx ppm	NO2 ppm	NO ppm	NOx ppm	NO2 ppm	Total HC	Methane			
1410	Internal	4.6	10.0															Water still in line
1430	Stack																	at 0900
1432				2.7	13.7	27	640		68								520	Water still in line
1447				2.9	13.7	22	625		69									at 0900
1502				2.7	13.6	20	624		70								520	
1517				2.6	13.7	18	640		70									
1532				2.7	13.6	17	632		69								520	
1602				2.8	13.4	16	631		67								527	
1547				2.7	13.5	18	636		67									
1617				2.8	13.4	19	639		69									
1632				2.7	13.4	17	643		68								528	
1647				2.8	13.5	15	652		72									
1702				2.8	13.4	15	649		72								537	
1717				2.7	13.4	15	656		73									
1732				2.9	13.4	15	657		71								540	
1747				2.8	13.4	13	664		71									
1802				2.9	13.4	15	675		70								537	
1817				2.9	13.4	9	675		67									
1832				2.9	13.4	13	691		70								533	
1847				2.8	13.4	12	692		72									
1902				2.4	13.6	13	697		70								531	
1917				2.8	13.5	13	697		70									
1932				2.7	13.6	12	713		69								528	
1947				2.6	13.7	12	715		70									
2002				2.8	13.4	12	705		68								534	
																		AVERAGE

4-34

ACUREX
Aerotherm

Load Range_____

[illegible]

FIELD DATA SHEET



Plant CHARLTON EER
 Location SUS - G9
 Operator MILBURN / Best
 Date 2-6-84
 Load Range _____

Ambient Temperature 67°F
 Barometric Pressure 29.52 (1115)
 Static Pressure Duct _____
 Fuel _____

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
0840	Open			+0.1	-0.2	0	+6		0										2 190
				7.39	16.1	165	512		87										CO 540 ppm
0900	internal expansion			7.25		185	553		90.1										SO ₂ 85 ppm
	cal																		Reactor back okay
0935	Start																		Black plume
0947				3.4	13.3	25	656		62										when CO high and
1002				2.8	13.9	14	657		60									435	migration when
1017				2.8	13.3	14	590		67										depleted CO on 1
1032				2.5	14.5	26	660		61									424	
1047				1.0	15.6	49	734		58										Unit operating at
1102				1.1	15.6	50	700		57									375	lower fuel rate
1117				1.0	15.5	28	698		57										
1132				0.9	15.7	55	714		58									374	
1147				0.8	15.6	80	701		55										
1202				0.7	15.8	35	768		55										
1217				2.6	14.6	28	636		54										
1232				2.8	14.4	23	628		55									392	
1247				2.8	14.4	25	627		56										
1302				2.8	14.2	18	627		54									417	
1317				2.9	14.2	27	624		55										
1332				2.7	14.2	30	626		55									427	
1347				2.6	14.7	23	627		54										
1402				2.8	14.5	25	618		55									426	
1417				2.9	14.4	24	617		55										
1432				3.0	14.2	22	658		54									426	
1447				2.8	14.6	4	645		55										AVERAGE
1502				2.4	14.2	11	712		55									413	

4-36

ACUREX
Aerotherm

Load Range_____

[illegible]

FIELD DATA SHEET



Plant Choron FFR
 Location SVS-69
 Operator Best/Melburn
 Date 2-7-84
 Load Range _____

Ambient Temperature 56°F 70°F
 Barometric Pressure 29.43 (0900) 29.32 (1500)
 Static Pressure Duct _____
 Fuel low grade

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED						CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC		
0800	internal & external calibration																	1020 smooth point
0830	Start																	< No. 1
0831				2.8	14.4	12	706		61								453	check back okay
0846				2.7	14.6	11	762		61									
0901				2.7	14.3	13	741		65								456	
0916				2.6	14.5	12	745		66									
0931				2.8	14.4	10	743		64								461	
0946				2.8	14.3	12	691		66									
1001				2.7	14.3	5	727		67								462	
1016				2.5	14.3	9	721		66									
1031				2.7	13.8	13	624		65								467	
1046				2.5	14.3	10	726		65									
1101				2.6	14.2	10	572		64								469	
1116				2.6	13.7	10	659		65									
1131				3.1	13.7	15	618		63								471	
1146				2.7	14.0	16	614		70									
1201				2.8	13.8	15	664		68								472	
1216				2.6	13.8	15	664		66									
1231				2.5	14.1	16	665		66								469	
1246				2.5	13.9	21	655		62									
1315				2.4	13.6	17	673		61								464	
1330				2.5	13.5	18	671		61									
1345				2.8	13.7	15	673		64								489	
1400				2.7	13.8	14	674		65									
1415				2.7	13.8	14	672		64								507	
1430				2.7	14.0	4	665		65									AVERAGE

4.38

FIELD DATA SHEET



Plant _____

Location _____

Operator _____

Date 2-7-84 (cont)

Load Range _____

Ambient Temperature _____

Barometric Pressure _____

Static Pressure Duct _____

Fuel _____

4-39

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H2O %	Stack Gas Temp °F	COMMENTS
				O2 %	CO2 %	CO ppm	SO2 ppm	NO ppm	NOx ppm	NO2 ppm	NO ppm	NOx ppm	NO2 ppm	Total HC	Methane	Non-Methane HC			
1445				2.6	14.0	5	665		64									504	
1500				2.8	14.0	6	651		65										
1508	internal span and recal			0.0	0.0	-20	0		+1										zero span gas valve
				7.1	17.3	165	620		88										
				7.25	18.15				90										
1535	start																		
1545				2.9	14.7	28	583		73									498	
1600				2.8	14.4	28	589		74										
1615				2.8	14.5	31	571		75									497	
1630				2.8	14.7	28	601		79										
1645				2.7	14.7	31	578		68									500	
1700				2.8	14.7	30	577		69										
1715				3.1	13.6	31	522		73									515	
1730				2.8	13.7	39	521		74										
1745				2.8	14.0	46	519		82									521	
1800				2.9	14.0	41	521		79										
1815				2.9	14.1	39	523		83									518	
1830				3.0	14.1	40	520		86										
1845				3.0	14.2	39	525		87									513	
1900				3.0	14.3	39	524		86										
1915				3.0	14.3	34	522		87									514	
1930				2.8	14.4	38	521		82										
1945				3.0	14.4	34	520		82									523	
2000				3.0	14.4	35	516		86										
2015				2.9	14.5	34	520		78									523	
2030				3.0	14.5	33	518		77										
AVERAGE																			

ACUREX
Aerotherm

Ambient Temperature _____

Barometric Pressure _____

Static Pressure Duct _____

Fuel _____

4-40

FIELD DATA SHEET

Plant Charcon (EER)
 Location SUS 69
 Operator M. Kurn / Best
 Date 2-8-84
 Load Range _____

Ambient Temperature 66 °F
 Barometric Pressure 29.33 (1430)
 Static Pressure Duct _____
 Fuel lease crude

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
0000				3.1	13.6	34	464		67										
0745	span internal																		flow loss
				10.1	10.3	120	115		10.7										span
				7.4	18.6	185	498		90.1										span
	calibrate internal & external			7.25	18.2	185	553		90.1										span gas
																			lock check okay
0955	start																		
1000				2.8	14.5	21	688		67										
1015				2.8	14.7	25	673		67									503	
1030				2.7	13.8	22	676		67										
1045				2.8	14.7	22	684		66									572	
1100				2.8	14.7	22	685		65										
1115				2.8	14.8	24	681		71									577	
1130				2.8	14.7	27	682		70										
1145				2.7	14.7	24	678		71									525	
1200				2.7	14.3	19	684		69										
1215				2.6	14.5	17	688		72									524	
1230				2.9	14.5	17	679		74										
1245				2.3	14.4	16	673		71									528	
1300				2.9	14.2	11	703		70										
1315				2.8	14.2	14	706		70									527	
1330				2.8	14.2	13	717		71										
1345				2.9	14.2	17	706		73									526	
1400				3.0	13.9	12	700		76										
1415				3.0	13.8	14	698		76									529	
																			AVERAGE

4-41

FIELD DATA SHEET



Plant _____
 Location _____
 Operator _____
 Date 2-8-84
 Load Range _____

Ambient Temperature _____
 Barometric Pressure _____
 Static Pressure Duct _____
 Fuel _____

4-42

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O ₂ DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
1430				2.4	14.3	9	722		73										
1445				2.8	14.3	11	699		73									532	
1500				2.7	14.1	12	700		70										
1515				2.8	14.0	14	673		66									526	
1530				3.2	13.8	18	637		63										
1545				3.0	13.8	18	635		62									519	x change in fuel rate
1600				3.1	13.7	15	631		63										
1615				3.2	13.5	16	622		61									518	
1630				3.2	13.6	18	630		61										
1645				3.1	14.4	23	627		61									519	
1700				3.2	13.9	21	633		63										
1715				3.2	13.4	20	635		66									524	
1730				3.2	13.7	23	642		67										
1745				3.2	13.5	22	642		77									534	
1800				3.4	13.5	18	629		77										
1815				3.2	13.6	19	643		75									537	
1830				3.3	14.0	20	630		80										
1845				3.2	13.7	21	629		80									533	
1900				2.9	13.3	18	639		70										
1915				3.1	13.8	18	638		65									535	
1930				3.2	13.8	21	629		73										
1945				3.2	13.9	21	633		65									533	
2000				3.2	13.9	22	625		63										
2015				3.2	13.9	24	631		62									525	
2030				3.2	13.9	21	633		64										
2045	Intermittent			0.0	-0.2	410	45		40.5									524	AVERAGE
				6.85	17.5	161	528		85										

FIELD DATA SHEET



Plant Chevron EER
 Location SUS 69
 Operator MILBURN
 Date 2-9-89
 Load Range _____

Ambient Temperature 65°F
 Barometric Pressure 29.27 (in Hg)
 Static Pressure Duct _____
 Fuel Lease Crude

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
0840	Internal and external calibration																		check stack temp
1000	Start																		
1006				3.2	13.9	17	529		73									537	
1021				3.1	13.8	17	539		70										
1036				3.1	13.8	17	549		69									538	
1051				2.9	13.7	14	554		66										
1106				3.1	13.8	23	554		66									533	
1121				3.0	13.6	17	539		64										
1136				2.9	13.8	17	549		67									521	
1151				2.8	14.1	16	544		68										
1206				2.9	14.0	16	539		68									520	
1221				3.1	13.9	15	544		68										
1236				2.9	14.1	15	549		68									523	
1251				2.9	14.0	15	544		69										
1306				3.0	13.7	19	559		64									524	
1321																			check NO ₂ zero
1336				2.8	13.7	21	579		71									523	
1351				2.7	13.6	22	579		69										
1406				2.8	13.7	21	559		65									531	
1421				2.8	13.5	20	584		66										
1436				3.0	13.4	16	559		65									536	
1451				2.9	13.5	16	605		74										
1506				3.1	13.4	14	619		75									538	
																			AVERAGE

FIELD DATA SHEET



Plant _____

Ambient Temperature _____

Location _____

Barometric Pressure _____

Operator _____

Static Pressure Duct _____

Date 2-9-84 (cont.)

Fuel _____

Load Range _____

4-44

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
1521				2.9	13.6	15	627		76										
1536				2.9	13.6	12	632		76									536	
1551				2.9	13.6	13	635		75										
1606				3.0	13.4	14	633		76									537	
1621				2.9	13.3	8	640		72										
1636				3.2	13.2	11	629		70									536	
1640	after 5 calif. mod			0.0	0.0	-5	+10		0										good
	internal			6.8	16.2	165	560		89										from
				7.2	18.4	183	545		90										stronger
1721				2.7	14.6	27	601		77										
1736				2.8	14.3	21	596		82									538	
1751				3.0	14.1	28	588		88										
1806				2.9	14.2	28	577		70									512	
1821				2.8	14.4	26	572		67										
1836				2.9	14.4	22	574		67									494	
1851				2.8	14.4	26	572		67										
1906				2.8	14.5	30	570		67									488	
1921				2.8	14.4	26	575		65										
1936				2.8	14.5	26	575		67									489	
1951				2.8	14.5	26	574		67										
2006				2.7	14.6	27	600		66									487	
2021				2.6	14.6	27	607		63										
2036				2.8	14.7	28	611		63									484	
																			AVERAGE

Load Range _____

[illegible]

FIELD DATA SHEET



Plant Chavon EER
 Location SUS 69
 Operator MILBURN
 Date 2-10-84
 Load Range _____

Ambient Temperature 60°F (1200)
 Barometric Pressure 29.43 (1200)
 Static Pressure Duct _____
 Fuel 1EASE Crude

4-46

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
0006				2.6	14.5	26	601		64									483	
0021				2.7	14.5	29	604		65										
0036				2.5	14.7	25	608		64									477	
0051				2.2	16.0	26	633		65										
0106				2.4	14.8	26	629		65									475	
0121				2.8	14.5	25	606		70									472	
0136				2.6	14.6	25	609		70										
0151				2.6	14.5	27	627		70									475	
0206				2.7	14.6	27	608		74										
0221				2.7	14.6	21	601		76									475	
0236				2.6	14.6	26	603		80										
0251				2.7	14.5	24	605		77									471	
0306				2.8	14.5	27	578		80										
0321				2.7	14.5	26	619		79									463	
0336				2.8	14.3	23	618		76										
0351				2.7	14.5	28	625		76									464	
0406				2.6	14.6	26	626		80										
0421				2.7	14.4	26	628		79									468	
0436				2.2	14.8	28	641		87										
0451				2.4	14.5	29	615		81									466	
0506				2.7	14.4	28	629		78										
0521				2.3	14.7	31	625		80									463	
0536				2.4	14.6	27	626		78										
0551				2.7	14.6	26	606		79									468	
0606				2.4	15.0	25	620		80										
																		AVERAGE	

FIELD DATA SHEET



Plant _____

Ambient Temperature _____

Location _____

Barometric Pressure _____

Operator _____

Static Pressure Duct _____

Date 2-10-84 (cont.)

Fuel _____

Load Range _____

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
0621				2.9	14.2	25	617		76										
0636				3.6	14.1	24	612		74									471	
0651				2.8	14.3	25	626		80										
0706	span																		
0721	span																		
0736	span																		
0751	span																		
0806	span																		
0821	span																		
0836	span																		
0851	span																		
0906	span																		
0921	span																		
0936	span																		
0951	span																		
1006	span																		
1021	span																		
1036	span																		
1051	span																		
1106	span																		
1121	span																		
1136	span																		
1151	span																		
AVERAGE																			

4-47

FIELD DATA SHEET



Plant _____
 Location _____
 Operator _____
 Date 2-10-84 (cont.)
 Load Range _____

Ambient Temperature _____
 Barometric Pressure _____
 Static Pressure Duct _____
 Fuel _____

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
1206				3.3	13.7	13	624		54									498	
1221				3.4	13.9	12	617		54										
1236				3.3	14.1	9	624		57									491	
1251				3.5	13.8	21	630		56										
1306				3.3	14.1	16	631		53									485	
1321				3.3	13.9	13	623		54										
1336				3.6	13.8	14	611		53									497	
1351				3.7	13.8	9	615		53										
1406				3.5	13.9	14	615		55									498	
1430	internal span and cal			0.0	0.0	-5	0		0										zero span span gas
				6.9	18.4	180	561		80										
				7.2	18.0	185	543		90.1										
1440	Start																		
1451				3.5	13.4	14	633		66										
1506				3.4	13.6	11	626		61									500	
1521				3.8	13.5	10	612		56										
1536				3.6	13.6	19	579		62									500	
1551				3.6	13.6	9	593		60										
1606				3.3	13.6	6	571		61									498	
1621				3.6	13.6	12	591		62										
1636				3.6	13.6	11	589		65									499	
1651				3.8	13.4	14	593		66										
1706				3.8	13.4	15	576		63									500	
1721				2.7	13.1	9	572		60										
1736				2.9	13.0	9	559		54									499	
1751				3.1	13.0	15	585		56										
1806				3.1	13.4	15	600		59										

↓
 Strachan

AVERAGE
 7 auto data gas
 5 ran out

ACUREX
Aerotherm

Ambient Temperature _____

Barometric Pressure _____

Static Pressure Duct _____

Fuel _____

4-49 ← strip chart

ACUREX
Aerotherm

Ambient Temperature 62°F
Barometric Pressure 29.40
Static Pressure Duct _____
Fuel 1st AC CRUDE

4-50

FIELD DATA SHEET



Plant Chescon (EEP)
 Location SUS-69
 Operator C. Milon
 Date 2-11-84
 Load Range _____

Ambient Temperature 62°F
 Barometric Pressure 29.90
 Static Pressure Duct _____
 Fuel 10450 C grade

4-51

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H2O %	Stack Gas Temp °F	COMMENTS
				O2 %	CO2 %	CO ppm	SO2 ppm	NO ppm	NOx ppm	NO2 ppm	NO ppm	NOx ppm	NO2 ppm	Total HC	Methane	Non-Methane HC			
0806				2.6	14.9	10.1	70.7		75									501	Corrected O2
0821				2.9	14.5	15.0	65.5		69.5									505	
0836				2.7	14.8	7.1	68.3		81.1									505	
0851				2.5	14.7	12.6	68.3		70.0									502	
0906				2.7	14.7	10.3	69.8		69.7									502	
0921				3.0	14.5	12.9	69.3		65.0									505	
1036				2.8	14.7	17.0	70.9		65.9									505	
1051				2.5	14.8	15.0	71.4		65.7									507	
1106				2.6	14.6	9.9	71.1		63.3									507	
1121				2.7	14.5	14.9	70.6		63.3									510	
1136				2.5	14.7	16.9	70.7		62.7									510	
1151				2.8	14.6	13.6	69.7		62.3									514	
1206				2.9	14.6	13.4	70.4		65.1									514	
1221				2.8	14.4	2.2	70.1		65.7									517	
1236				2.9	14.4	14.6	69.8		66.7									517	
1251				2.8	14.5	8.0	70.0		66.0									516	
1306				2.7	14.5	15.1	70.7		65.6									516	
1321				2.5	14.6	19.7	69.3		66.1									510	
1336				2.4	14.5	12.8	70.6		66.8									510	
1351				2.7	14.3	15.5	68.6		65.9									510	
1406				2.9	14.2	14.3	66.6		63.7									510	
1421				2.7	14.3	14.0	66.2		65.6									509	
1436				2.9	14.0	20.4	65.1		65.3									509	
1451				2.8	14.1	13.7	63.5		63.6									507	
1506				2.7	14.1	22.5	62.4		62.3									507	
																			AVERAGE

FIELD DATA SHEET



Plant Chemson (CCR)
 Location SUS 69
 Operator C.M. LUNA
 Date 2-11-84
 Load Range _____

Ambient Temperature 62°F
 Barometric Pressure 29.41
 Static Pressure Duct _____
 Fuel house crude

4-52

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
1521																			Calibrate 1520-1530
1536				2.7	14.2	14.7	544		62.8									505	O ₂ 2.5% O ₂ SPAN 2.0%
1551				2.4	14.4	25.8	571		63.4										CO ₂ " 0% " 17.9%
1606				2.6	14.3	18.4	643		61.1									502	CO " 60ppm " 1220ppm
1621				2.7	13.8	26.9	630		62.1									506	SO ₂ " 10.1ppm " 490ppm
1636				2.6	13.5	20.9	632		63.9										NO _x " 0ppm " 89ppm
1651				2.6	13.5	15.7	634		65.4										
1706				2.5	13.6	24.7	638		65.2									506	RECAL
1721				2.4	13.6	19.3	639		64.9										
1736				2.3	14.0	18.4	656		41.6									500	
1751				2.5	14.0	25.2	648												NO _x (last sample Fl.)
1806				2.7	13.6	17.7	642											501	
1821				2.7	13.8	18.0	660												
1836				2.4	13.7	18.6	686											492	
1851				2.4	13.4	14.0	679												
1906				2.6	13.8	19.1	681											490	
1921				2.8	13.6	16.4	683												
1936				2.5	13.8	14.6	700											491	
1951				2.5	14.6	16.8	694		67.9										
2006				2.4	14.6	20.2	692		74.2									499	
2021				2.6	14.6	9.5	707		69.4										
2036				2.7	14.5	20.7	713		68.6									504	
2051				2.4	14.8	10.8	733		73.4										
2106				2.4	15.5	17.5	731		75.3									497	
2121				2.4	15.1	17.8	731		78.3										
																			AVERAGE

ACUREX
Aerotherm

Ambient Temperature 63° F

Barometric Pressure 29.40

Static Pressure Duct _____

Fuel Lease Crude

4-53

ACUREX
Aerotherm

Ambient Temperature _____
Barometric Pressure _____
Static Pressure Duct _____
Fuel 1-Base Crude

4-54

FIELD DATA SHEET



Plant Cherson (eer)
 Location SVS 69
 Operator C.M. Buch
 Date 2-15/84
 Load Range _____

Ambient Temperature _____
 Barometric Pressure _____
 Static Pressure Duct _____
 Fuel _____

4-55

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED						CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC		
1705				3.3	13.5		558		69.7								445	Accelerator came
1718				2.8	14.3		575		770									Back on at 1830
1733				2.9	13.7		549		75.6								447	2-15-84
1748				3.0	13.3		543		72.8									
1803				2.9	13.3		554		72.8								446	Lost CO monitor
1818				2.9	13.2		557		62.2									
1833				3.1	13.0		550		61.8								459	O ₂ subject to drift
1848				3.1	13.3		555		61.2									
1903				3.0	13.3		557		59.9								463	
1918				3.2	13.4		560											NOx Analyzer trouble
1933				3.2	13.6		559										465	
1948				3.3	13.9		556											CO Gas - 65
2003				3.2	14.5		565										466	
2018				3.2	14.5		565											CO ₂ 18.15%
2033				3.3	14.6		560											O ₂ 7.25%
2048				3.5	13.9		562		61.9								466	SO ₂ 548 ppm
2103				3.4	13.8		540		60.7									NOx 96.1 ppm
2118				3.2	14.1		542		62.4									
2133				3.3	14.3		560		62.0								468	
2148				3.3	14.3		565		61.5									
2203				3.2	14.5		564		63.1								467	
2218				3.3	14.4		564		65.2									
2233				3.4	14.4		565		63.4								469	
2248				3.7	14.3		560		64.9									
2303				3.3	14.4		554		63.8								469	
																		AVERAGE

ACUREX
Aerotherm

Ambient Temperature _____

Barometric Pressure _____

Static Pressure Duct _____

Fuel _____

[illegible]

FIELD DATA SHEET



Plant Chouron (eer)
 Location SUS 69
 Operator C. Milburn
 Date 2-16-84
 Load Range _____

Ambient Temperature _____
 Barometric Pressure _____
 Static Pressure Duct _____
 Fuel _____

4-57

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O ₂ DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
0003				3.0	14.6		554		59.5									463	CAL GAS
0018				3.2	14.4		519		59.5										O ₂ = 7.20%
0033				2.9	14.5		623		54.5									462	CO ₂ = 18.00%
0048				2.8	14.6		613		60.3										SO ₂ = 54.3 ppm
0103				3.3	14.3		546		58.3									408	NO _x = 90.1 ppm
0118				3.1	14.3		573		60.2										
0133				3.1	14.3		565		59.7									465	CO ₂ OFF STACK CHECK
0148				3.3	13.9		545		60.9										
0203				3.4	14.0		534		63.6									472	
0218				3.3	14.0		542		63.2										SPAN CHECK
0233				3.3	14.1		540		62.4									468	
0248				3.3	14.2		554		60.7										ZERO SPAN
0303				3.4	14.2		557		62.5									471	O ₂ 0.90 4.49%
0318				3.3	14.3		556		63.6										CO ₂
0333				3.3	14.3		557		63.6									467	SO ₂
0348				3.2	14.3		560		62.9										NO _x .3 ppm 86 ppm
0403				3.2	14.2		560		65.5									467	
0418				3.2	14.3		566		65.5										
0433				3.2	14.5		569		68.5									460	
0448				3.2	14.4		571		65.5										
0503				3.2	14.4		553		66.5									459	
0518				3.2	14.2		554		69.0										
0533				3.2	14.1		529		68.4									461	
0548				3.2	13.9		531		71.8										
0603				3.2	13.9		483		71.6										
																			AVERAGE

ACUREX
Aerotherm

Ambient Temperature _____

Barometric Pressure _____

Static Pressure Duct _____

Fuel _____

4-58

FIELD DATA SHEET



Plant Chevron
 Location SUS-69
 Operator MIEBURN
 Date 2-22-84
 Load Range _____

Ambient Temperature 63°F
 Barometric Pressure 29.410
 Static Pressure Duct _____
 Fuel LEASE crude

4-59

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
1029				3.2	12.7		648		72.1									543	1029 to 1344 OFF -
1044				2.9	14.1		645		72.6										Strip charts - NO
1059				3.2	12.7		636		78.6									546	Auto data paper
1114				3.0	10.0		637		80.1										
1129				3.0	15.4		629		80.9									553	Cal Gases
1144				3.1	15.0		627		82.0										O ₂ 7.20 %
1159				3.0	13.0		622		82.1									559	NO _x 90.1 ppm
1214				3.1	10.1		621		80.0										SO ₂ 530 ppm - I could
1229				2.9	8.8		619		77.2									556	not reach the
1244				3.0	16.7		631		75.7										SPAN OF 543 Because
1259				3.0	16.9		617		75.5									563	The Instrument could not
1314				2.5	15.0		606		75.0										SPAN
1329				2.4	15.0		651		71.7										CO ₂ 18.14 %
1344				2.5	14.2		660		70.0										
1359				2.6	14.3		637		68.8									532	SPAN CHECK
1414				2.5	13.8		640		68.6										O ₂ 2.00 % SPAN 6.45 %
1429				2.6	13.3		645		71.7									529	NO _x 86.3 ppm
1444				2.3	13.1		661		71.4										SO ₂ 440 ppm 523 ppm
1459				END TEST															CO ₂ -1.2 % 16.2 %
1514				2.7	14.3		654		67.3										
1529				2.5	14.4		680		74.5										
1544				2.4	13.9		683		73.1										
1559				2.7	13.5		665		70.8										
1614				2.8	13.4		670		67.0										
																			AVERAGE

FIELD DATA SHEET



Plant Chevron (FER)
 Location SUS 69
 Operator C. N. BURN
 Date 2-22-84
 Load Range _____

Ambient Temperature _____
 Barometric Pressure _____
 Static Pressure Duct _____
 Fuel _____

4-60

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
1629				2.7	13.4		664		70.0										
1644				2.5	13.4		684		76.4										
1659				2.8	13.1		662		74.1										
1714				2.8	13.0		671		74.0										
1729				2.8	13.0		678		76.2										
1744				2.7	13.1		681		76.7										
1759				3.1	12.8		660		72.0										
1814				2.6	13.2		685		71.2										
1829				2.7	13.2		684		68.0										
1844				2.8	13.3		675		69.1										
1859				2.9	13.3		677		64.6										
1914				2.7	13.6		686		74.4										
1929				2.8	13.6		683		72.8										
1944				2.8	13.7		688		73.8										
1959				Onion Temping															
2014				2.3	13.6		724		72.5							0			
2029				2.8	13.6		681		72.8							0			
2044				2.6	13.5		692		70.3							0			
2059				2.6	13.2		684		67.8							0			
2114				2.7	13.0		670		66.1							0			
2129				2.5	12.9		698		68.4							0			
2144				2.7	12.7		692		64.5							0			
2159				2.6	12.6		683		66.2							0			
2214				2.5	12.6		688		68.7							0			
2229				2.7	12.2		686		71.4							0			
																			AVERAGE

ACUREX
Aerotherm

Ambient Temperature _____

Barometric Pressure _____

Static Pressure Duct _____

Fuel _____

19-4

FIELD DATA SHEET



Plant Chevron
 Location SUS-69
 Operator MILBURN
 Date 2-23-84
 Load Range _____

Ambient Temperature 63°F
 Barometric Pressure 29.40
 Static Pressure Duct _____
 Fuel Lease Crude

4-62

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED						CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC		
0014				2.6	11.1		670		72.6							0		
0029				2.9	10.4		659		70.4							0		
0044				2.7	11.0		674		72.7							0		
0059				2.7	10.8		678		68.6							0		
0114				2.7	10.7		680		73.1							0		
0129				2.7	10.5		666		72.0							0		
0144				2.8	10.3		660		72.8							0		
0159				2.8	10.1		663		75.5							0		
0214				2.8	10.2		660		75.4							0		
0229				2.9	10.0		652		76.4							0		
0244				2.8	9.8		664		76.0							0		
0259				2.7	9.8		668		72.2							0		
0314				2.5	9.8		654		71.6							0		
0329				2.6	9.7		650		70.5							0		
0344				2.7	9.5		657		69.8							0		
0359				2.8	9.6		674		69.3							0		
0414				2.9	9.4		663		65.4							0		
0429				2.9	9.4		660		69.8							0		
0444				2.9	9.3		651		67.8							0		
0459				2.9	9.3		660		68.8							0		
0514				3.1	9.2		648		72.9							0		
0529				3.1	9.2		656		70.2							0		
0544				3.1	9.2		640		70.5							0		
0559				3.0	9.2		648	412	60.6	676						0		
0614				3.0	9.1		634		67.5							0		
AVERAGE																		

FIELD DATA SHEET



Plant Chescon (ccr)
 Location SUS C9
 Operator C. A. Brown
 Date 2-23-84
 Load Range _____

Ambient Temperature _____
 Barometric Pressure _____
 Static Pressure Duct _____
 Fuel _____

4-63

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H ₂ O %	Stack Gas Temp °F	COMMENTS
				O ₂ %	CO ₂ %	CO ppm	SO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	NO ppm	NO _x ppm	NO ₂ ppm	Total HC	Methane	Non-Methane HC			
0634				3.1	8.4		617		70.6										O ₂ Subject to Drift
0644				3.0	8.9		560		67.9										Zero SPAN
0654				Test over															O ₂ 1.9% 70%
				reagent															CO ₂ 10.5% 18.15
0839				2.6	15.6		608		74.4										SO ₂ 5 ppm 495
0914				2.7	15.8		602		76.7										NO _x 0.1 ppm 82 ppm
0929				2.8	16.9		601		75.9										
0944				2.9	16.3		602		70.6										
0959				2.9	17.6		598		70.1										
1014				2.8	18.5		628		68.7										
1029				3.3	14.5		644		72.4										
1044				3.3	14.7		648		72.6										
1059				3.3	12.5		641		72.3										
1114				3.2	12.2		657		68.3										
1129				→	16.6		477		→									548	Check O ₂ Cal
1144				3.5	14.6		547		69.1										
1159				3.5	16.4		614		69.5									549	
1214				3.6	17.4		621		66.4										
1229				3.7	17.2		631		68.8									537	
1244				3.7	14.0		655		69.2										
1259				4.0	14.5		645		65.9									545	Zero SPAN
1314				4.4	14.5		649		67.9										O ₂ 0% 6.95%
1329				4.8	14.0		626		70.4									553	CO ₂ 10% 19.3%
1344				4.9	13.5		634		72.1										SO ₂ 16 ppm 548 ppm
1359																			NO _x 0.1 ppm 86.5 ppm
																			AVERAGE

FIELD DATA SHEET



Plant Cherwon (EER)
 Location SUS 69
 Operator MILBURN
 Date 2-24-84
 Load Range _____

Ambient Temperature 66°F
 Barometric Pressure 29.40
 Static Pressure Duct _____
 Fuel 1 case crude

Time	Sample Point	Load MW	Steam Flow lb/hr x1000	DRY UNCORRECTED							CORRECTED TO 3% O2 DRY			HYDROCARBONS (HC)			H2O %	Stack Gas Temp °F	COMMENTS
				O2 %	CO2 %	CO ppm	SO2 ppm	NO ppm	NOx ppm	NO2 ppm	NO ppm	NOx ppm	NO2 ppm	Total HC	Methane	Non-Methane HC			
804				2.2						75									O2 meter suspect / 10
0950				2.2	12.8		689			707								544	DRIFT C804-1244
1005				2.2	13.16		688			713								535	
1020				2.3	12.78		641			713								527	
1035				2.6	13.12		630			701								535	
1040				3.0	12.93		627			683								530	
1105				3.1	12.50		630			710								531	
1120				3.2	13.05		632			687								527	
1135				3.3	12.34		622			692								527	
1150				3.3	12.3		622			694									
1205				3.3	12.7		637			654								544	
1220					11.9		637			649									
1235					12.6		636			691								547	
1250				2.7	11.2		635			726									
1305				2.7	11.8		632			742								547	O2 OFF strip chart
1320				2.7	11.8		636			718									
1335				2.6	12.2		642			704								549	zero span
1350				2.7	11.7		625			740									O2 0% 7.75%
1405				2.7	12.2		631			714								548	CO2 - 1% 17.05%
1420				2.8	12.0		635			727									SO2 - 10ppm 490ppm
1435				2.7	11.7		637			665								543	NOx 0ppm 87.6ppm
1450				2.7	11.9		668			728									
1505				2.7	12.2		629			734								553	
1620				Test over															
AVERAGE																			

4-64

4.2 FIELD DATA SHEETS FOR EPA METHOD 5/8, SASS, VOST, ANDERSEN IMPACTOR,
CONTROLLED CONDENSATION (CCS), AND EPA METHOD 7

Page 1 of 2

Probe Length and Type 5' glass
 Nozzle Size & I.D. .309 A-100 Clear
 Pitot Coefficient & I.D. _____
 Assumed Moisture 11 _____
 Molecular Weight, Dry, (M_d) _____
 Meter Box Number D555 _____
 Meter Coefficient .679 _____
 α Factor 0.915 _____
 $K =$ 935.06 _____
 $K(N_d)^4 =$ _____ $\times$ (_____)⁴ = _____
 $\Delta H = K(N_d)^4 \left(\frac{T_m}{T_s} \right) (P)$

SASS Condensate _____
Total Volume _____

4-66	Traverse Point Number	Sampling Time, min	Clock Time (24-hr) Clock	Gas Meter Reading (V _m), ft ³	Velocity Head (AP _s), in. H ₂ O	Orifice Pressure Differential (ΔH), in. H ₂ O		Temperature of							Pump Vacuum in. Hg	Avg. $\bar{P}$
						Desired	Actual	Stack	Probe	Impinger	Organic Module	Oven	Gas Meter			
													In	Out		
			1124	Init. 720.987												
	12	0.0		720.987	.37	1.81	1.8	457	227	37		204	65	65	7	
	11	3.0		723.21	.45	2.18	2.2	466	232	36		214	66	68	10	
	10	6.0		725.55	.49	2.27	2.3	465	237	36		256	69	67	10	
	9	9.0		727.98	.45	2.18	2.2	464	236	38		255	69	67	10	
	8	12.0		730.44	.45	2.21	2.2	465	227	38		256	69	67	10	
	7	15.0		732.83	.45	2.21	2.2	456	229	42		256	69	66	10	
	6	18.0		735.24	.45	2.21	2.2	454	230	45		255	68	65	11	
	5	21.0		738.44	.40	1.77	2.0	455	232	46		255	67	65	11	
	4	24.0		739.96	.35	1.72	1.7	456	234	46		257	68	65	11	

7602/5/E Rev 1

Comments:

4-67

Traverse Point Number	Clock Time (24-hr) Clock		Gas Meter Reading (V _m), ft ³	Velocity Head (ΔP _s), in. H ₂ O	Orifice Pressure Differential (ΔH), in. H ₂ O		Temperature of					Gas Meter		Pump Vacuum in. Hg	Avg. √ΔP
	Sampling Time, min	Init.			Desired	Actual	Stack	Probe	Impinger	Organic Module	Oven	In	Out		
3	27.0	742.13	.35	1.72	1.7	456	232	45		256	68	65	10		
2	30.0	744.25	.35	1.72	1.7	454	233	46		255	68	65	10		
1	33.0	746.39	.25	1.23	1.2	450	231	48		254	67	65	8		
	36.0-End	748.276													
12	36.0 1216	748.276	.50	2.46	2.4	453	227	52		266	68	67	15		
11	39.0	750.77	.50	2.46	2.4	454	232	47		261	72	69	15		
10	42.0	753.45	.50	2.49	2.5	454	231	48		259	74	71	11		
9	45.0	756.15	.48	2.39	2.4	453	235	52		261	78	71	11		
8	48.0	758.66	.47	2.34	2.3	453	238	52		268	76	72	11		
7	51.0	761.12	.45	2.24	2.2	454	238	55		269	74	72	10		
6	54.0	763.54	.45	2.25	2.2	453	242	54		270	76	73	10		
5	57.0	765.93	.43	2.10	2.10	453	239	55		271	75	72	10		
4	60.0	768.34	.45	2.25	2.2	454	237	54		272	76	73	10		
3	63.0	770.71	.45	2.25	2.2	452	235	54		268	76	73	10		
2	66.0	773.11	.45	2.25	2.2	450	237	54		266	76	72	11		
1	69.0	775.64	.25	1.25	1.3	450	235	54		264	76	72	8		

72.06 m/s

777.625

(0.649)

2.075 456.2

69.9

Purge train for 15 minutes at 10 A.H.

Run No.

1

56.638

Date

2-1-84

Sampling Location

Outlet

Comments:

(v_{ap})

Impinger Volumes		
Initial	Final	Net Gain
500.0	534.3	34.3
538.1	601.2	43.1
530.0	559.0	29.0

Silica Gel		
560.9	584.0	23.1

Probe Length and Type 5' glass
Nozzle Size & I.D. 309 P-100 dry
Pitot Coefficient & I.D. _____
Assumed Moisture 11
Molecular Weight, Dry, (M_d) _____
Meter Box Number 2555
Meter Coefficient 0.677
 α Factor 99.5
 $K =$ _____
 $K(N_d)^4 =$ _____ $\times$ (_____)⁴ = _____
 $\Delta H = K(N_d)^4 \left(\frac{T_m}{T_s} \right) (P)$

SASS Condensate N/A
Total Volume 129.5

Traverse Point Number	Sampling Time, min	Clock Time (24-hr) Clock	Gas Meter Reading (V_m), ft ³	Velocity Head (ΔP), in. H ₂ O	Orifice Pressure Differential (ΔH), in. H ₂ O		Temperature of						Pump Vacuum in. Hg	Avg. ΔP	
					Desired	Actual	Stack	Probe	Impinger	Organic Module	Oven	Gas Meter			
												In			Out
12	0.0	1940	Intt. 787.417												
12	0.0		787.417	.43	2.07	2.1	472	252	58			243	67	66	7
11	3.0		789.78	.43	2.07	2.1	472	248	48			256	68	66	7
10	6.0		792.31	.50	2.40	2.4	472	231	58			272	72	71	8
9	9.0		794.43	.48	2.31	2.3	473	235	52			271	73	69	7
8	12.0		796.86	.50	2.44	2.4	473	242	56			279	74	72	7
7	15.0		799.46	.45	2.19	2.2	472	244	62			245	76	72	8
6	18.0		801.90	.43	2.11	2.1	473	235	67			235	78	74	8
5	21.0		804.33	.45	2.20	2.2	475	238	65			234	79	75	8
4	24.0		806.79	.45	2.21	2.2	474	234	60			235	80	77	8

7602/5/E Rev 1

Comments:

Traverse Point Number	Clock Time (24-hr) Clock	Gas Meter Reading (V _m), ft ³	Velocity Head (ΔP _s), in. H ₂ O	Orifice Pressure Differential (ΔH), in. H ₂ O		Temperature of					Gas Meter		Pump Vacuum in. Hg	Avg. √ΔP
						Stack	Probe	Impinger	Organic Module	Oven	In	Out		
	Sampling Time, min	Init.	Desired	Actual										
3	27.0	809.17	.45	2.21	2.2	476	242	56		258	81	77	8	
2	30.0	811.60	.45	2.22	2.2	475	242	56		265	81	78	8	
1	33.0	814.04	.45	2.22	2.2	474	248	48		273	81	78	8	
	36.0 82.0	816.476												
12	South 21.60	816.476	.47	2.29	2.3	488	298	49		280	80	82	8	
11	39.0	818.96	.45	2.19	2.2	487	265	51		243	84	83	8	
10	42.0	821.34	.50	2.44	2.4	490	258	55		238	85	83	8	
9	45.0	823.80	.50	2.45	2.4	485	253	55		233	84	82	9	
8	48.0	826.34	.50	2.45	2.4	486	248	54		271	84	81	9	
7	51.0	828.87	.50	2.44	2.4	485	243	53		267	83	81	9	
6	54.0	831.39	.45	2.20	2.2	483	231	53		267	83	81	9	
5	57.0	833.85	.42	2.05	2.1	483	235	52		269	82	80	9	
4	60.0	836.26	.43	2.05	2.1	482	241	51		269	80	78	9	
3	63.0	838.63	.40	1.95	1.9	483	238	50		262	80	78	8	
2	66.0	840.96	.40	1.95	1.9	483	240	50		263	80	78	8	
1	69.0	843.36	.30	1.46	1.5	482	241	49		267	79	77	7	
	72.0 End	845.360												

57.943 16696 (V_{ΔP}) 2.18 479.1

(77.8) ÷ 48

Run No. 2Date 2-1-84Sampling Location OutletComments: Average for 15 minutes at 1.0 AH

Page 1 of 2

SASS Condensate 1920
Total Volume

Traverse Point Number	Sampling Time, min	Clock Time (24-hr) Clock	Gas Meter Reading (V_m), ft ³	Velocity Head ($4P_s$), in. H ₂ O	Orifice Pressure Differential (ΔH), in. H ₂ O		Temperature °F							Pump Vacuum in. Hg	Avg. $\bar{u}$ /ft	
					Desired	Actual	Stack	Probe	Impinger	Organic Module	Oven	Gas Meter				
												In	Out			
	0	1129	Init. 73.411													
	10		111.5	.45	2.10	2.1	454	319			48	395	78	78	18	.671
	20		148.1	.40	1.87	1.9	450	396			50	402	78	77	17	.632
	30		183.9	.46	1.86	1.9	451	407			49	405	84	78	17	.632
	40		219.3	.40	1.90	1.9	450	411			50	407	87	81	19	.632
	50		254.4	.40	1.91	1.7	451	409			52	408	92	84	20	.632
	60	1233	290.9	.40	1.91	1.9	451	409			54	325	90	89	12	.632
	70		326.3	.40	1.92	1.9	450	409			51	342	92	89	16	.632
	80		362.4	.40	1.93	1.9	450	409			51	364	97	91	17	.632
	90		400.6	.40	1.93	1.9	454	409			51	375	99	94	18	.632

min. 31 - drain condensate from Org. Mod. min 61 - Drain condensate
Comments: min 50 - stop to change filters restart 1233

7602/5/E Rev 1

Traverse Point Number	Clock Time (24-hr) Clock	Gas Meter Reading (V _m), ft ³	Velocity Head (ΔP _s), in. H ₂ O	Orifice Pressure Differential (ΔH), in. H ₂ O		Temperature of					Gas Meter		Pump Vacuum in. Hg	Avg. √ΔP
						Stack	Probe	Impinger	Organic Module	Oven	In	Out		
	Sampling Time, min	Init. 400.6	Desired	Actual										
	90													
	100	435.2	.40	1.94	1.9	457	409		51	383	104	96	20	.632
	110	470.7	.40	1.94	1.7	454	408		50	377	98	98	20	.632
	120 1400	506.0	.40	1.94	1.7	450	409		52	370	99	97	20	.632
	130	542.0	.40	1.94	1.9	449	404		75	325	95	95	14	.632
	140 1442	580.7	.40	1.94	1.9	448	404		72	406	95	94	15	.632
	150	616.0	.40	1.94	1.9	449	412		54	409	97	95	17	.632
	160	651.8	.46	1.95	1.9	448	413		54	407	101	96	18	.632
	170	687.1	.40	1.92	1.8	467	406		51	410	103	97	20	.632
	180 1521	721.6	.40	1.91	1.6	470	406		52	409	104	98	20	.632
	190	758.1	.40	1.90	1.9	466	406		57	362	94	98	14	.632
	200	795.1	.40	1.91	1.9	466	412		53	343	96	97	16	.632
	210	832.7	.40	1.91	1.9	466	414		54	333	101	97	19	.632
	220	868.6	.40	1.93	1.9	463	415		56	369	103	99	20	.632
	230	904.6	.40	1.93	1.8	463	414		56	371	104	99	20	.632
	240	939.830	.40	1.93	1.7	463	406		56	369	103	99		.632
		866.42	0.40	1.93	1.9	456								0.632

Run No. SASS 1Date 2/1/84Sampling Location Boiler outlet

Min 110 - stop to change filter Restart 1400
 Comments: Min 121 - Drain condensate

Min 140 - stop to change S.G. Restart 1422
 Min 152 - Drain Condensate
 Min 180 - stop to change filter Restart 1521

Min 185 - Drain Condensate

Min 240 - stop to change filter Restart

Stop test - filter holder connection galled,
 cannot remove filter holder

4-71

Volatile Organic Sampling Sampling Train (VOST) Data Sheet

Plant Chevron (EER) / CMEA

Project No. 307735.81

Date 2-1-84

Operator M. M. MURRAY

Sample Location Sec. 27 Unit 39 STACK

Barometric Pressure (in. Hg) 29.28 (2pr)

Run No. 1 (TRAPS packed in culture tubes)

Ambient Temperature (°F) 60

Trap Set	Trap I.D.	Clock Time 24 Hour	Elapsed Time (minutes)	Dry Gas Meter (L)	Volume Sampled (L)	Temperature (°F)				Rotometer Setting	Pump Vacuum (in. Hg)	Leak Rate LPM at Vacuum	Comments
						DGM	Probe	Heated Line	Tenax Inlet				
A	45	Start: 1530	42	0.00	21.188	70	370	N/A	57	40	<1	0.05@	68°F before 2nd trap
	19A	Stop: 1612		21.188		78	354	N/A	62	40	<1	15" Hg	84°F before 2nd trap
B	23	Start: 1814	40.5	0.00	20.140	64	331	N/A	52	40	<1	0.07 LPM@	61°F before 2nd trap
	24A	Stop: 20		20.14		68	316	N/A	64	38	<1	15" Hg	68°F " " "
C	9	Start: 1730	N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A	Trap Blank
	35A	Stop: -		N/A		N/A	N/A	N/A	N/A	N/A	N/A	N/A	
D	11	Start: N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A	Field Blank
	32A	Stop: N/A		N/A		N/A	N/A	N/A	N/A	N/A	N/A	N/A	
E	21	Start: 1825	41.1	0.00	20.151	62	365	N/A	52	40	0.5	0.04@	75°F before 2nd TRAP
	13A	Stop: 1906		20.151		70	345	N/A	57	37	5	10" Hg	69°F before 2nd trap
F		Start:											
		Stop:											
Summary													

Notes: ^{a)} 2nd knockout impinger added after test set A (wouldn't seal properly for set A & was wrapped in TFE tape for test B)
^{b)} After set A, noticed charcoal fines in 1st Condenser (probably from charcoal purge trap). Condenser was changed out to clean one.
^{c)} Culture tube broke & lost 1/4" cap for trap #45; 1/4" cap lost from 19A ^{d)} sudden increase in stack moisture during set B
^{e)} SET E - 1st trap has significant moisture - not noted with other sets (After 15 mins of test)

Volatile Organic Sampling Train (VOST) Data Sheet

Plant CHEVRON/EEB (AMEA)
 Date 2/1/84
 Sample Location Sec 27 Unit 39 STARK
 Run No. 2 (traps in cigar boxes)

Project No. 307135.80
 Operator Murray
 Barometric Pressure (in. Hg) 29.28
 Ambient Temperature (°F) 60

Trap Set	Trap I.D.	Clock Time 24 Hour	Elapsed Time (minutes)	Dry Gas Meter (L)	Volume Sampled (L)	Temperature (°F)				Rotometer Setting	Pump Vacuum (in. Hg)	Leak Rate LPM at Vacuum	Comments
						DGM	Probe	Heated Line	Tenax Inlet				
A	42	Start: 1901	N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A	TRIP BLANK N
	15A	Stop: N/A		N/A		N/A	N/A	N/A	N/A	N/A	N/A	N/A	
B	70	Start: 1945	39.7	0.00	20.01	62	312	N/A	67	40	1	0.06 @ 11"	61° before 2nd trap
	33A	Stop: 2025		20.01		70	316	N/A	69	2/0	1	Hg	66°F before 2nd trap
C	40	Start: 1940	N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A	FIELD BLANK
	1A	Stop: N/A		N/A		N/A	N/A	N/A	N/A	N/A	N/A	N/A	
D		Start:											
		Stop:											
E		Start:											
		Stop:											
F		Start:											
		Stop:											
Summary	X	X		X								X	X

Notes:

ANDERSEN FIELD TEST DATA

Plant Chemex (FER) Date 2-22-84 Ambient Temperature _____ °F
 Test Location SVS-69 Out Operator Best Barometric Pressure 29.36 " Hg
 Run No. 1 Nozzle Size & No. .250 Static Pressure (P_g) -0.25" H₂O " Hg
 Molecular Weight _____ Pitot Coefficient .82 Filter Set No. UOP-23
 % H₂O _____ Pitot No. _____ Meter Box No. #105
 Orifice Coefficient .67 x 1.001

C.99cmf

SAMPLE POINT NUMBER	CLOCK TIME SAMPLE TIME	VELOCITY HEAT ΔP in. wg.	ORIFICE METER ΔH in. wg.	GAS METER VOLUME FT ³	TEMPERATURES °F			GAS METER		PUMP VACUUM in. Hg	√ΔP	COMMENTS
					STACK	PROBE	IMPINGER	IN	OUT			
6	11:4 0.0	.4.8	0.9	945.646	549			67	67	5	.663	initial leak rate
	5.0		0.9	948.23				65	66	5		.008 gpm at 10" Hg
	10.0		0.9	950.70				65	67	5.5		pre heat impactor
	15.0		0.9					64	65	6		20 min in stack
	20.0		0.9	955.58				64	64	6.5		
	25.0		0.9	957.08	556			64	64	7		
	30.0			960.628								
	30.15											Final leak rate
												0.009 at 10" Hg
AVERAGE TOTAL	30.15		0.9	14982	552.5			64.8	65.5			

902229

902227

(65.2)

ANDERSEN FIELD TEST DATA

Plant Chavara (CEER)

Date 2-22-84

Ambient Temperature _____ °F

Test Location SV5-69 outlet

Operator Bart

Barometric Pressure 29.32 " Hg

Run No. 2

Nozzle Size & No. 250

Static Pressure (P_s) -0.25" H_2O 419

Molecular Weight _____

Pitot Coefficient .82

Filter Set No. UOP-20

% H₂O _____

Pitot No. _____

Meter Box No. 105

Orifice Coefficient .67

SAMPLE POINT NUMBER	CLOCK TIME SAMPLE TIME	VELOCITY HEAT ΔP in. wg.	ORIFICE METER ΔH in. wg.	GAS METER VOLUME FT ³	TEMPERATURES °F					PUMP VACUUM In. Hg	√ΔP	COMMENTS
					STACK	PROBE	IMPINGER	GAS METER				
								IN	OUT			
6	1352 0.0	.94	0.9	960.875	532			61	59	5	.663	initial leak rate
	6.0		0.9	963.36				60	59	6		.005 cfm at 10" Hg
	10.0		0.9	965.79				61	59	6		Preheat impinger
	15.0		0.9	968.22				60	59	6.5		20 min. in stack
	20.0		0.9	970.67				61	58	7		
	25.0		0.9	973.11				63	58	7		
	30.0	End		975.55 /	53 /							Final leak rate
												.007 cfm at 10" Hg

(57.8)

**CONTROLLED CONDENSATION SYSTEM (CCS)
FIELD DATA SHEET**

Plant Clavon EFR
 Date 2-23-84
 Sample Location SVS-69 Outlet
 Run No. 1
 Operator Best

Ambient Temperature _____
 Barometric Pressure 29.34
 Meter Box Number 105
 Meter Orifice Coefficient .67
 Meter α Factor 1.000

*initial
leak rate
.003 cfm
at 10" Hg
(nozzle)*

Sampling Time, min	Clock Time (24-hr) clock	Gas Meter Reading (V _m), ft ³	Temperature (°F)								Dry Gas Meter		AH wg
			Stack	④ Probe	Filter		② Recirc Water	① Exit Coil					
		③ Skin			⑤ Out								
						Init.			In	Out			
		975.729											
0.0	1243	975.729	537	575	1053	565	144	143	71	69	0.4	6	
5.0				566	1140	700	148	147	69	67	0.4	6	
10.0		779.18		559	796	581	150	148	68	67	0.4	6	
15.0		980.88		579	857	514	149	147	68	67	0.4	6.5	
20.0		984.40		586	1226	706	149	147	67	67	0.4	7	
25.0		984.40		595	1396	783	149	147	67	66	0.4	7	
30.0		986.12		591	865	583	149	147	67	67	0.4	7	
35.6		987.90		592	893	516	149	147	67	65	0.4	7	
40.0		989.51		597	1200	685	149	147	67	65	0.4	8	
45.0		991.27		586	787	534	150	148	67	66	0.4	8	
50.0		993.1		587	736	501	149	147	66	66	0.4	9	
55.0		994.71		589	1151	694	149	147	66	66	0.4	9	
60.0 End		996.444							67.8	66.5			
				902292				902296					
Average		20.715							67.4				

*Final
leak rate
.007 at
10" Hg*

**CONTROLLED CONDENSATION SYSTEM (CCS)
FIELD DATA SHEET**

Plant Chuvon CEER Ambient Temperature _____
 Date 2-23-84 Barometric Pressure 29.32
 Sample Location SVS-69 Outlet Meter Box Number 105
 Run No. 2 Meter Orifice Coefficient .67
 Operator Best Meter & Factor 1.000

*initial back
rate
at 10" Hg
sample*

Clock Time (24-hr) clock	Gas Meter Reading (V _m), ft ³	Temperature (°F)								4 H	Avg H _g
		Stack	(4) Probe	Filter		① Recirc Water	② Exit Coil	Dry Gas Meter			
				(3) Skin	(5) Out			In	Out		
Sam- pling Time, min	Init.										
	996.577										
0.0 1737	996.577	449	527	1232	475	153	145	64	64	0.4	8
5.0	998.42		576	1271	532	159	143	63	65	0.4	7
10.0	018.90		577	1224	577	153	145	64	65	0.4	7
15.0	018.90		577	1220	562	153	145	64	64	0.4	7
20.0	003.63		582	1212	553	154	146	64	64	0.4	8
25.0	005.36		576	1183	530	154	146	62	62	0.4	8
30.0	007.10		585	1320	535	154	146	62	62	0.4	9
35.0	010.67		580	1331	523	154	146	62	62	0.4	9.5
40.0	010.67		580	1252	511	154	146	62	62	0.4	10
45.0	012.44		582	1231	544	153	145	58	59	0.4	10
50.0	014.16		577	1290	497	153	145	58	59	0.4	10
55.0	015.85		574	1222	486	153	145	57	58	0.4	10
60.0 End	017.561										
Average	20.924							61.5	61.9	0.4	

*Final back
rate
at 10" Hg*

902301

902302

902297

4-77 902293

902300

902298

Run Number 1
 Date 1-24-84

NO_x SAMPLINGPROBE

<u>Unit No.</u>	<u>Length =</u>		<u>Lining Material</u>	<u>Pre-Filter</u>	<u>Heated</u>	<u>Pitot Tube</u>
<u>N/A</u>	<u>3</u>	ft	☐ S. Steel	☒ Glass Wool	☒ Yes	No. <u>N/A</u>
			☒ Pyrex	☐ _____	☐ No	Coefficient:
						☐ .85 ☐ <u>N/A</u>

SAMPLING DATA

Flask No.	<u>2</u>	<u>25</u>	<u>18</u>	_____
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Volume of Flask Less Absorb. Soln.	<u>2032</u>	<u>2087</u>	<u>2079</u>	_____
---------------------------------------	-------------	-------------	-------------	-------

Initial Conditions:

Barometric Pressure (in. Hg)	<u>29.65</u>	<u>29.65</u>	<u>29.65</u>	_____
Flask Temperature (°F)	<u>70</u>	<u>70</u>	<u>72</u>	_____
Flask Vacuum (in. Hg):				_____
Top	<u>13.2</u>	<u>16.2</u>	<u>15.9</u>	_____
Bottom	<u>16.2</u>	<u>13.1</u>	<u>13.2</u>	_____
Difference	<u>29.4</u>	<u>29.3</u>	<u>29.1</u>	_____
Leak Check	<u>OK</u>	<u>OK</u>	<u>OK</u>	_____

Sampling Location:

Port	<u>Directly above cm port</u>	_____	_____
Point or Distance from Inside of Port	<u>~1.5'</u>	<u>1.5'</u>	<u>1.5'</u>
Clock Time	<u>1101</u>	<u>1116</u>	<u>1132</u>

Performed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	_____
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Comments:

Probe Temp = 406°F

Run Number 1NO_x SAMPLE RECOVERY
AND ANALYSISSAMPLE RECOVERY

Flask No.	<u>2</u>	<u>25</u>	<u>18</u>	<u> </u>
Final Conditions:				
Barometric Pressure (in. Hg)	<u>29.50</u>	<u>29.50</u>	<u>29.50</u>	<u> </u>
Flask Temperature (°F)	<u>64</u>	<u>71</u>	<u>72</u>	<u> </u>
Flask Vacuum (in. Hg):				
Top	<u>0.2</u>	<u>0.2</u>	<u>0.5</u>	<u> </u>
Bottom	<u>0.8</u>	<u>0.2</u>	<u>0.7</u>	<u> </u>
Difference	<u>1.0</u>	<u>0.4</u>	<u>1.2</u>	<u> </u>
Sample Number	<u>901398</u>	<u>901399</u>	<u>901400</u>	<u> </u>
Date	<u>1-25-84</u>	<u>1-25-84</u>	<u>1-25-84</u>	<u> </u>
Clock Time	<u>1048</u>	<u>1455</u>	<u>1128</u>	<u> </u>
Performed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	<u> </u>

ANALYSIS

Analysis Procedure

Spectrophotometric

Sample Number	<u>901398</u>	<u>901399</u>	<u>901400</u>	<u> </u>
Absorbance of Sample	<u>0.170</u>	<u>0.209</u>	<u>0.161</u>	<u> </u>
Absorbance of Blank	<u>0</u>	<u>0</u>	<u>0</u>	<u> </u>
Calibration Curve No.	<u>1</u>	<u>1</u>	<u>1</u>	<u> </u>
Mass of NO _x as NO ₂ (μg)	<u>250.0</u>	<u>307.3</u>	<u>236.7</u>	<u> </u>
Analysis Date	<u>3-15-84</u>	<u>3-15-84</u>	<u>3-15-84</u>	<u> </u>
Analyzed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	<u> </u>

Comments:

Run Number 2
 Date 1-24-84
NO_x SAMPLINGPROBE

<u>Unit No.</u>	<u>Length =</u>	<u>Lining Material</u>	<u>Pre-Filter</u>	<u>Heated</u>	<u>Pitot Tube</u>
	<u>3</u> ft	☐ S. Steel ☒ Pyrex	☒ Glass Wool ☐ _____	☒ Yes ☐ No	No. <u>N/A</u> Coefficient: ☐ .85 ☐ <u>N/A</u>

SAMPLING DATA

Flask No.	<u>7</u>	<u>8</u>	<u>6</u>	
Volume of Flask Less Absorb. Soln.	<u>2046</u>	<u>1995</u>	<u>2062</u>	
Initial Conditions:				
Barometric Pressure (in. Hg)	<u>29.65</u>	<u>29.65</u>	<u>29.65</u>	
Flask Temperature (°F)	<u>68</u>	<u>70</u>	<u>80</u>	
Flask Vacuum (in. Hg):				
Top	<u>16.2</u>	<u>13.2</u>	<u>16.2</u>	
Bottom	<u>13.2</u>	<u>16.2</u>	<u>13.2</u>	
Difference	<u>29.4</u>	<u>29.4</u>	<u>29.4</u>	
Leak Check	<u>OK</u>	<u>OK</u>	<u>OK</u>	
Sampling Location:				
Port	<u>directly above cm port</u>			
Point or Distance from Inside of Port	<u>1.5'</u>	<u>1.5'</u>	<u>1.5'</u>	
Clock Time	<u>1201</u>	<u>1216</u>	<u>1232</u>	
Performed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	

Comments:

probe temp = 406°F

Run Number 2 **NO_x SAMPLE RECOVERY AND ANALYSIS**

SAMPLE RECOVERY

Flask No.	<u>7</u>	<u>8</u>	<u>6</u>	
Final Conditions:				
Barometric Pressure (in. Hg)	<u>29.44</u>	<u>29.44</u>	<u>29.44</u>	
Flask Temperature (°F)	<u>72</u>	<u>74</u>	<u>74</u>	
Flask Vacuum (in. Hg):				
Top	<u>0.2</u>	<u>0.3</u>	<u>0.3</u>	
Bottom	<u>0.2</u>	<u>0.3</u>	<u>0.5</u>	
Difference	<u>0.4</u>	<u>0.6</u>	<u>0.8</u>	
Sample Number	<u>901401</u>	<u>901402</u>	<u>901403</u>	
Date	<u>1-25-84</u>	<u>1-25-84</u>	<u>1-25-84</u>	
Clock Time	<u>1500</u>	<u>1430</u>	<u>1452</u>	
Performed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	

ANALYSIS

Analysis Procedure	<u>Spectrophotometric</u>			
Sample Number	<u>901401</u>	<u>901402</u>	<u>901403</u>	
Absorbance of Sample	<u>0.211</u>	<u>0.359</u>	<u>0.275</u>	
Absorbance of Blank	<u>0</u>	<u>0</u>	<u>0</u>	
Calibration Curve No.	<u>1</u>	<u>1</u>	<u>1</u>	
Mass of NO _x as NO ₂ (μg)	<u>620.5</u>	<u>1055.7</u>	<u>808.7</u>	
Analysis Date	<u>3-15-84</u>	<u>3-15-84</u>	<u>3-15-84</u>	
Analyzed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	
Comments:				

ACUREX CORPORATION

 Run Number 3
 Date 1-24-84
NO_x SAMPLINGPROBE

<u>Unit No.</u>	<u>Length =</u>	<u>ft</u>	<u>Lining Material</u>	<u>Pre-Filter</u>	<u>Heated</u>	<u>Pitot Tube</u>
<u>N/A</u>	<u>3</u>		☐ S. Steel ☒ Pyrex	☒ Glass Wool ☐ _____	☒ Yes ☐ No	No. <u>N/A</u> Coefficient: ☐ .85 ☐ <u>N/A</u>

SAMPLING DATA

Flask No.	<u>5</u>	<u>4</u>	<u>13</u>	
Volume of Flask				
Less Absorb. Soln.	<u>1989</u>	<u>2023</u>	<u>2075</u>	
Initial Conditions:				
Barometric Pressure (in. Hg)	<u>29.58</u>	<u>29.58</u>	<u>29.58</u>	
Flask Temperature (°F)	<u>80</u>	<u>75</u>	<u>78</u>	
Flask Vacuum (in. Hg):				
Top	<u>15.9</u>	<u>16.1</u>	<u>13.1</u>	
Bottom	<u>13.2</u>	<u>13.1</u>	<u>16.0</u>	
Difference	<u>29.1</u>	<u>29.2</u>	<u>29.1</u>	
Leak Check	<u>OK</u>	<u>OK</u>	<u>OK</u>	
Sampling Location:				
Port	<u>directly above CM PORT</u>			
Point or Distance from				
Inside of Port	<u>1.5'</u>	<u>1.5'</u>	<u>1.5'</u>	
Clock Time	<u>1301</u>	<u>1316</u>	<u>1331</u>	
Performed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	

Comments:

Probe temp = 390°F

Run Number 3NO_x SAMPLE RECOVERY
AND ANALYSISSAMPLE RECOVERY

Flask No.	<u>5</u>	<u>4</u>	<u>13</u>	
Final Conditions:				
Barometric Pressure (in. Hg)	<u>29.50</u>	<u>29.5</u>	<u>29.5</u>	
Flask Temperature (°F)	<u>62</u>	<u>73</u>	<u>64</u>	
Flask Vacuum (in. Hg):				
Top	<u>0.6</u>	<u>0.5</u>	<u>0.2</u>	
Bottom	<u>0.3</u>	<u>0.1</u>	<u>0.3</u>	
Difference	<u>0.9</u>	<u>0.2</u>	<u>0.5</u>	
Sample Number	<u>901404</u>	<u>901405</u>	<u>901406</u>	
Date	<u>8-25-84</u>	<u>1-25-84</u>	<u>1-25-84</u>	
Clock Time	<u>1111</u>	<u>1446</u>	<u>1050</u>	
Performed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	

ANALYSIS

Analysis Procedure

Spectrophotometric

	<u>901404</u>	<u>901405</u>	<u>901406</u>	<u>901406</u>
Sample Number				
Absorbance of Sample	<u>0.169</u>	<u>0.150</u>	<u>0.282</u>	<u>0.248</u>
Absorbance of Blank	<u>0</u>	<u>0</u>	<u>0</u>	<u>0</u>
Calibration Curve No.	<u>1</u>	<u>1</u>	<u>1</u>	<u>1</u>
Mass of NO _x as NO ₂ (μg)	<u>248.5</u>	<u>220.5</u>	<u>829.3</u>	<u>729.3</u>
Analysis Date	<u>3-15-84</u>	<u>3-15-84</u>	<u>3-15-84</u>	<u>3-15-84</u>
Analyzed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>

Comments:

Sample recovery - slight sample loss during recovery of #13 & #4

ACUREX CORPORATION

Run Number 4
Date 1-24-84NO_x SAMPLINGPROBE

<u>Unit No.</u>	<u>Length =</u>		<u>Lining Material</u>	<u>Pre-Filter</u>	<u>Heated</u>	<u>Pitot Tube</u>
<u>N/A</u>	<u>3</u> ft		☐ S. Steel	☒ Glass Wool	☒ Yes	No. <u>N/A</u>
			☒ Pyrex	☐ _____	☐ No	Coefficient:
						☐ .85 ☐ <u>N/A</u>

SAMPLING DATA

Flask No.	<u>46</u>	<u>9</u>	<u>14</u>	
Volume of Flask Less Absorb. Soln.	<u>2082</u>	<u>2077</u>	<u>2049</u>	
Initial Conditions:				
Barometric Pressure (in. Hg)	<u>29.54</u>	<u>29.54</u>	<u>29.54</u>	
Flask Temperature (°F)	<u>74</u>	<u>75</u>	<u>76</u>	
Flask Vacuum (in. Hg):				
Top	<u>16.2</u>	<u>16.1</u>	<u>16.1</u>	
Bottom	<u>13.2</u>	<u>13.2</u>	<u>13.0</u>	
Difference	<u>29.4</u>	<u>29.3</u>	<u>29.1</u>	
Leak Check	<u>OK</u>	<u>OK</u>	<u>OK</u>	
Sampling Location:				
Port	<u>directly above cm port</u>			
Point or Distance from Inside of Port	<u>1.5'</u>	<u>1.5'</u>	<u>1.5'</u>	
Clock Time	<u>1401</u>	<u>1416</u>	<u>1431</u>	
Performed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	

Comments:

probe temp = 428°F

Run Number 4NO_x SAMPLE RECOVERY
AND ANALYSISSAMPLE RECOVERY

Flask No.	<u>46</u>	<u>9</u>	<u>14</u>	_____
Final Conditions:				
Barometric Pressure (in. Hg)	<u>29.50</u>	<u>29.5</u>	<u>29.5</u>	_____
Flask Temperature (°F)	<u>70</u>	<u>72</u>	<u>64</u>	_____
Flask Vacuum (in. Hg):				
Top	<u>1.2</u>	<u>0.6</u>	<u>0.8</u>	_____
Bottom	<u>1.0</u>	<u>0.7</u>	<u>0.4</u>	_____
Difference	<u>2.2</u>	<u>1.3</u>	<u>1.2</u>	_____
Sample Number	<u>901407</u>	<u>901408</u>	<u>901409</u>	_____
Date	<u>1-25-84</u>	<u>1-25-84</u>	<u>1-25-84</u>	_____
Clock Time	<u>1155</u>	<u>1450</u>	<u>1109</u>	_____
Performed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	_____

ANALYSISAnalysis Procedure Spectrophotometric

Sample Number	<u>901407</u>	<u>901408</u>	<u>901409</u>	_____
Absorbance of Sample	<u>0.188</u>	<u>0.109</u>	<u>0.138</u>	_____
Absorbance of Blank	<u>0</u>	<u>0</u>	<u>0</u>	_____
Calibration Curve No.	<u>1</u>	<u>1</u>	<u>1</u>	_____
Mass of NO _x as NO ₂ (µg)	<u>276.4</u>	<u>160.3</u>	<u>202.9</u>	_____
Analysis Date	<u>3-15-84</u>	<u>3-15-84</u>	<u>3-15-84</u>	_____
Analyzed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	_____

Comments:

~~Pr~~ slight loss of sample in recovery of #46

ACUREX CORPORATION

 Run Number 5
 Date 1-24-84
NO_x SAMPLINGPROBE

<u>Unit No.</u>	<u>Length =</u>		<u>Lining</u> <u>Material</u>	<u>Pre-Filter</u>	<u>Heated</u>	<u>Pitot</u> <u>Tube</u>
<u>N/A</u>	<u>3</u> ft		☐ S. Steel ☒ Pyrex	☒ Glass Wool ☐ _____	☒ Yes ☐ No	No. <u>N/A</u> Coefficient: ☐ .85 ☒ <u>N/A</u>

SAMPLING DATA

Flask No.	<u>45</u>	<u>10</u>	<u>30</u>	_____
Volume of Flask Less Absorb. Soln.	<u>2075</u>	<u>2060</u>	<u>2006</u>	_____
Initial Conditions:				
Barometric Pressure (in. Hg)	<u>29.54</u>	<u>29.54</u>	<u>29.54</u>	_____
Flask Temperature (°F)	<u>76</u>	<u>72</u>	<u>72</u>	_____
Flask Vacuum (in. Hg):				
Top	<u>16.0</u>	<u>15.9</u>	<u>16.1</u>	_____
Bottom	<u>13.1</u>	<u>13.0</u>	<u>13.1</u>	_____
Difference	<u>29.1</u>	<u>28.9</u>	<u>29.2</u>	_____
Leak Check	<u>OK</u>	<u>OK</u>	<u>OK</u>	_____
Sampling Location:				
Port	<u>directly above cm port</u>			
Point or Distance from Inside of Port	<u>1.5'</u>	<u>1.5'</u>	<u>1.5'</u>	_____
Clock Time	<u>1501</u>	<u>1516</u>	<u>1531</u>	_____
Performed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	_____

Comments:

Run Number 5NO_x SAMPLE RECOVERY
AND ANALYSISSAMPLE RECOVERY

Flask No.	<u>45</u>	<u>10</u>	<u>30</u>	<u> </u>
Final Conditions:				
Barometric Pressure (in. Hg)	<u>29.5</u>	<u>29.5</u>	<u>29.5</u>	<u> </u>
Flask Temperature (°F)	<u>66</u>	<u>73</u>	<u>65</u>	<u> </u>
Flask Vacuum (in. Hg):				
Top	<u>0.9</u>	<u>0.2</u>	<u>0.8</u>	<u> </u>
Bottom	<u>0.6</u>	<u>0.8</u>	<u>1.0</u>	<u> </u>
Difference	<u>1.5</u>	<u>1.0</u>	<u>1.8</u>	<u> </u>
Sample Number	<u>901410</u>	<u>901411</u>	<u>901412</u>	<u> </u>
Date	<u>8-25-84</u>	<u>1-25-84</u>	<u>1-25-84</u>	<u> </u>
Clock Time	<u>1213</u>	<u>1446</u>	<u>1156</u>	<u> </u>
Performed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	<u> </u>

ANALYSIS

Analysis Procedure	<u>Spectrophotometric</u>			
Sample Number	<u>901410</u>	<u>901411</u>	<u>901412</u>	<u> </u>
Absorbance of Sample	<u>0.112</u>	<u>0.200</u>	<u>0.082</u>	<u> </u>
Absorbance of Blank	<u>0</u>	<u>0</u>	<u>0</u>	<u> </u>
Calibration Curve No.	<u>1</u>	<u>1</u>	<u>1</u>	<u> </u>
Mass of NO _x as NO ₂ (μg)	<u>164.71</u>	<u>294.1</u>	<u>120.6</u>	<u> </u>
Analysis Date	<u>3-15-84</u>	<u>3-15-84</u>	<u>3-15-84</u>	<u> </u>
Analyzed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	<u> </u>
Comments:				

ACUREX CORPORATION

 Run Number 6
 Date 1-24-84
NO_x SAMPLINGPROBE

<u>Unit No.</u>	<u>Length =</u>		<u>Lining</u> <u>Material</u>	<u>Pre-Filter</u>	<u>Heated</u>	<u>Pitot</u> <u>Tube</u>
<u>N/A</u>	<u>3</u>	ft	☐ S. Steel ☒ Pyrex	☒ Glass Wool ☐ _____	☒ Yes ☐ No	No. <u>N/A</u> Coefficient: ☐ .85 ☐ <u>N/A</u>

SAMPLING DATA

Flask No.	<u>17</u>	<u>F52</u>	<u>21</u>	_____
Volume of Flask Less Absorb. Soln.	<u>2012</u>	<u>2043</u>	<u>2081</u>	_____
Initial Conditions:				
Barometric Pressure (in. Hg)	<u>29.54</u>	<u>29.54</u>	<u>29.54</u>	_____
Flask Temperature (°F)	<u>72</u>	<u>72</u>	<u>74</u>	_____
Flask Vacuum (in. Hg):				
Top	<u>13.1</u>	<u>16.2</u>	<u>16.2</u>	_____
Bottom	<u>16.0</u>	<u>13.0</u>	<u>13.1</u>	_____
Difference	<u>29.1</u>	<u>29.2</u>	<u>29.3</u>	_____
Leak Check	<u>OK</u>	<u>OK</u>	<u>OK</u>	_____
Sampling Location:				
Port	<u>directly above cm port</u>			
Point or Distance from Inside of Port	<u>1.5'</u>	<u>1.5'</u>	<u>1.5'</u>	_____
Clock Time	<u>1601</u>	<u>1616</u>	<u>1631</u>	_____
Performed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	_____

Comments:

probe temp = 484°F

Run Number 6 NO_x SAMPLE RECOVERY AND ANALYSIS

SAMPLE RECOVERY

Flask No.	<u>17</u>	<u>F52</u>	<u>21</u>	<u> </u>
Final Conditions:				
Barometric Pressure (in. Hg)	<u>29.46</u>	<u>29.46</u>	<u>29.46</u>	<u> </u>
Flask Temperature (°F)	<u>72</u>	<u>72</u>	<u>74</u>	<u> </u>
Flask Vacuum (in. Hg):				
Top	<u>0.2</u>	<u>0.3</u>	<u>0.3</u>	<u> </u>
Bottom	<u>0.1</u>	<u>0.1</u>	<u>0.2</u>	<u> </u>
Difference	<u>0.3</u>	<u>0.4</u>	<u>0.5</u>	<u> </u>
Sample Number	<u>901413</u>	<u>901414</u>	<u>901415</u>	<u> </u>
Date	<u>1-25-84</u>	<u>1-25-84</u>	<u>1-25-84</u>	<u> </u>
Clock Time	<u>1315</u>	<u>1310</u>	<u>1430</u>	<u> </u>
Performed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	<u> </u>

ANALYSIS

Analysis Procedure	<u>Spectrophotometric</u>			
Sample Number	<u>901413</u>	<u>901414</u>	<u>901415</u>	<u> </u>
Absorbance of Sample	<u>0.141</u>	<u>0.235</u>	<u>0.122</u>	<u> </u>
Absorbance of Blank	<u>0</u>	<u>0</u>	<u>0</u>	<u> </u>
Calibration Curve No.	<u>1</u>	<u>1</u>	<u>1</u>	<u> </u>
Mass of NO _x as NO ₂ (μg)	<u>207.31</u>	<u>345.5</u>	<u>179.4</u>	<u> </u>
Analysis Date	<u>3-15-84</u>	<u>3-15-84</u>	<u>3-15-84</u>	<u> </u>
Analyzed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	<u> </u>
Comments:				

ACUREX CORPORATION

Run Number 7
Date 1-24-84NO_x SAMPLINGPROBE

<u>Unit No.</u>	<u>Length =</u>	<u>Lining Material</u>	<u>Pre-Filter</u>	<u>Heated</u>	<u>Pitot Tube</u>
<u>N/A</u>	<u>3</u> ft	☐ S. Steel ☒ Pyrex	☒ Glass Wool ☐ _____	☒ Yes ☐ No	No. <u>N/A</u> Coefficient: ☐ .85 ☐ <u>N/A</u>

SAMPLING DATA

Flask No.	<u>1</u>	<u>22</u>	<u>2A</u>	_____
Volume of Flask Less Absorb. Soln.	<u>1996</u>	<u>2045</u>	<u>2011</u>	_____
Initial Conditions:				
Barometric Pressure (in. Hg)	<u>29.54</u>	<u>29.54</u>	<u>29.54</u>	_____
Flask Temperature (°F)	<u>66</u>	<u>65</u>	<u>65</u>	_____
Flask Vacuum (in. Hg):				
Top	<u>16.1</u>	<u>16.2</u>	<u>16.2</u>	_____
Bottom	<u>12.9</u>	<u>13.0</u>	<u>13.1</u>	_____
Difference	<u>29.0</u>	<u>29.2</u>	<u>29.3</u>	_____
Leak Check	<u>OK</u>	<u>OK</u>	<u>OK</u>	_____
Sampling Location:				
Port	<u>directly above Cm port</u>			
Point or Distance from Inside of Port	<u>1.5'</u>	<u>1.5'</u>	<u>1.5'</u>	_____
Clock Time	<u>1701</u>	<u>1716</u>	<u>1731</u>	_____
Performed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	_____

Comments:

probe = 426°F

Run Number 7NO_x SAMPLE RECOVERY
AND ANALYSISSAMPLE RECOVERY

Flask No.	<u>1</u>	<u>22</u>	<u>2A</u>	<u> </u>
Final Conditions:				
Barometric Pressure (in. Hg)	<u>29.46</u>	<u>29.46</u>	<u>29.46</u>	<u> </u>
Flask Temperature (°F)	<u>71</u>	<u>70</u>	<u>71</u>	<u> </u>
Flask Vacuum (in. Hg):				
Top	<u>0.0</u>	<u>0.1</u>	<u>0.6</u>	<u> </u>
Bottom	<u>0.3</u>	<u>0.1</u>	<u>0.6</u>	<u> </u>
Difference	<u>0.3</u>	<u>0.2</u>	<u>1.2</u>	<u> </u>
Sample Number	<u>901416</u>	<u>901417</u>	<u>901418</u>	<u> </u>
Date	<u>1-25-84</u>	<u>1-25-84</u>	<u>1-25-84</u>	<u> </u>
Clock Time	<u>1235</u>	<u>1515</u>	<u>1530</u>	<u> </u>
Performed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	<u> </u>

ANALYSIS

Analysis Procedure

Spectrophotometric

Sample Number	<u>901416</u>	<u>901417</u>	<u>901418</u>	<u> </u>
Absorbance of Sample	<u>0.131</u>	<u>0.315</u>	<u>0.151</u>	<u> </u>
Absorbance of Blank	<u>0</u>	<u>0</u>	<u>0</u>	<u> </u>
Calibration Curve No.	<u>1</u>	<u>1</u>	<u>1</u>	<u> </u>
Mass of NO _x as NO ₂ (µg)	<u>192.6</u>	<u>926.3</u>	<u>222.0</u>	<u> </u>
Analysis Date	<u>3-15-84</u>	<u>3-15-84</u>	<u>3-15-84</u>	<u> </u>
Analyzed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	<u> </u>

Comments:

Flask #22 had styrofoam peanut in flask

ACUREX CORPORATION

 Run Number 8
 Date 1-24-84
NO_x SAMPLINGPROBE

<u>Unit No.</u>	<u>Length =</u>	<u>Lining Material</u>	<u>Pre-Filter</u>	<u>Heated</u>	<u>Pitot Tube</u>
<u>N/A</u>	<u>3</u> ft	☐ S. Steel ☒ Pyrex	☒ Glass Wool ☐ _____	☒ Yes ☐ No	No. <u>N/A</u> Coefficient: ☐ .85 ☐ <u>N/A</u>

SAMPLING DATA
 Flask No. 6A 20 43 _____

 Volume of Flask
 Less Absorb. Soln. _____ 2041 2053 _____

Initial Conditions:

Barometric Pressure (in. Hg)	<u>29.54</u>	<u>29.54</u>	<u>29.54</u>	_____
Flask Temperature (°F)	<u>67</u>	<u>68</u>	<u>68</u>	_____
Flask Vacuum (in. Hg):				
Top	<u>16.2</u>	<u>16.2</u>	<u>16.2</u>	_____
Bottom	<u>13.1</u>	<u>13.1</u>	<u>13.0</u>	_____
Difference	<u>29.3</u>	<u>29.3</u>	<u>29.2</u>	_____
Leak Check	<u>OK</u>	<u>OK</u>	<u>OK</u>	_____

Sampling Location:

Port	<u>directly above CM port</u>			_____
Point or Distance from				
Inside of Port	<u>1.5'</u>	<u>1.5'</u>	<u>1.5'</u>	_____
Clock Time	<u>1801</u>	<u>1820</u>	<u>1835</u>	_____

 Performed by mmm mmm mmm _____

Comments:

CM Filter change @ 1815
 probe temp = 419°F

Run Number 8NO_x SAMPLE RECOVERY
AND ANALYSISSAMPLE RECOVERYFlask No. 6A 20 43

Final Conditions:

Barometric Pressure (in. Hg) 29.5 29.5 29.5Flask Temperature (°F) 68 72 71

Flask Vacuum (in. Hg):

Top 0.1 0.2 0.3Bottom 0.3 0.3 0.2Difference 0.4 0.5 0.5Sample Number 901419 901420 901422Date 1-25-84 1-25-84 1-25-84Clock Time 1235 1455 1330Performed by mmm mmm mmmANALYSISAnalysis Procedure SpectrophotometricSample Number 901419 901420 901422Absorbance of Sample 0.078 0.161 0.135Absorbance of Blank 0 0 0Calibration Curve No. 1 1 1Mass of NO_x as NO₂ (µg) 114.7 236.7 198.5Analysis Date 3-15-84 3-15-84 3-15-84Analyzed by mmm mmm mmm

Comments:

ACUREX CORPORATION

 Run Number 9
 Date 1-24-84
NO_x SAMPLINGPROBE

<u>Unit No.</u>	<u>Length =</u>	<u>Lining</u> <u>Material</u>	<u>Pre-Filter</u>	<u>Heated</u>	<u>Pitot</u> <u>Tube</u>
<u>N/A</u>	<u>3</u> ft	☐ S. Steel ☒ Pyrex	☒ Glass Wool ☐ _____	☒ Yes ☐ No	No. <u>N/A</u> Coefficient: ☐ .85 ☐ <u>N/A</u>

SAMPLING DATA

Flask No.	<u>19</u>	<u>23</u>	<u>F51</u>	_____
Volume of Flask Less Absorb. Soln.	<u>2064</u>	<u>2037</u>	<u>2053</u>	_____
Initial Conditions:				
Barometric Pressure (in. Hg)	<u>29.54</u>	<u>29.54</u>	<u>29.54</u>	_____
Flask Temperature (°F)	<u>62</u>	<u>62</u>	<u>63</u>	_____
Flask Vacuum (in. Hg):				_____
Top	<u>16.3</u>	<u>16.2</u>	<u>16.3</u>	_____
Bottom	<u>13.0</u>	<u>13.1</u>	<u>13.0</u>	_____
Difference	<u>29.3</u>	<u>29.3</u>	<u>29.3</u>	_____
Leak Check	<u>OK</u>	<u>OK</u>	<u>OK</u>	_____
Sampling Location:				
Port	<u>directly above dm port</u>			_____
Point or Distance from Inside of Port	<u>1.5'</u>	<u>1.5'</u>	<u>1.5'</u>	_____
Clock Time	<u>1905</u>	<u>1920</u>	<u>1936</u>	_____
Performed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	_____

Comments:

Probe temp = 487°F

Run Number 9NO_x SAMPLE RECOVERY
AND ANALYSISSAMPLE RECOVERY

Flask No.	<u>19</u>	<u>23</u>	<u>F51</u>	
Final Conditions:				
Barometric Pressure (in. Hg)	<u>29.46</u>	<u>29.46</u>	<u>29.46</u>	
Flask Temperature (°F)	<u>66</u>	<u>66</u>	<u>71</u>	
Flask Vacuum (in. Hg):				
Top	<u>16.3</u>	<u>16.2</u>	<u>16.3</u>	
Bottom	<u>13.0</u>	<u>13.1</u>	<u>13.0</u>	
Difference	<u>29.3</u>	<u>29.3</u>	<u>29.3</u>	
Sample Number	<u>901422</u>	<u>901423</u>	<u>901424</u>	
Date	<u>1-25-84</u>	<u>1-25-84</u>	<u>1-25-84</u>	
Clock Time	<u>1139</u>	<u>1215</u>	<u>1137</u>	
Performed by	<u>mmm</u>	<u>mmm</u>	<u>mmm</u>	

ANALYSIS

Analysis Procedure	<u>Spectrophotometric</u>			
Sample Number	<u>901422</u>	<u>901423</u>	<u>901424</u>	
Absorbance of Sample	<u>0.121</u>	<u>0.072</u>	<u>0.102</u>	
Absorbance of Blank	<u>0</u>	<u>0</u>	<u>0</u>	
Calibration Curve No.	<u>1</u>	<u>1</u>	<u>1</u>	
Mass of NO _x as NO ₂ (µg)	<u>177.9</u>	<u>105.9</u>	<u>150.0</u>	
Analysis Date				
Analyzed by				
Comments:				

PLANT *Chorron (CCR)* OPERATOR *Best*

LOCATION *SIS 69 outlet*

DATE *2-8-84*

TIME

AMBIENT PRESSURE (IN. HG.) *INIT 29.37 FINAL 29.35*

AMBIENT TEMPERATURE (°F)

SAMPLING POINT *30" above CM*

TEST NUMBER *pen 1*

NO_x SAMPLING DATA

Time	Flask Number	Flask Volume (ml.)	Initial Conditions		Final Conditions	
			Flask Vacuum (in. Hg.)	Flask Temp (°F)	Flask Vacuum (in. Hg.)	Flask Temp (°F)
<i>1055</i>	<i>30</i>	<i>2006</i>	<i>29.0</i>	<i>55</i>	<i>0.9</i>	<i>58</i>
<i>1110</i>	<i>46</i>	<i>2082</i>	<i>28.7</i>	<i>63</i>	<i>1.2</i>	<i>58</i>
<i>1130</i>	<i>17</i>	<i>2012</i>	<i>29.0</i>	<i>60</i>	<i>1.4</i>	<i>59</i>

PLANT *Chlorine (E22)*OPERATOR *Best*LOCATION *SUS 69 outlet*DATE *2-8-84*

TIME

INIT FIN
AMBIENT PRESSURE (IN. HG.) *29.37* *29.25*

AMBIENT TEMPERATURE (°F)

SAMPLING POINT *30" above CH*TEST NUMBER *Run 2*NO_x SAMPLING DATA

Time	Flask Number	Flask Volume (ml.)	Initial Conditions		Final Conditions	
			Flask Vacuum (in. Hg.)	Flask Temp (°F)	Flask Vacuum (in. Hg.)	Flask Temp (°F)
<i>1155</i>	<i>13</i>	<i>2075</i>	<i>28.5</i>	<i>79</i>	<i>2.1</i>	<i>59</i>
<i>1210</i>	<i>14</i>	<i>2049</i>	<i>28.7</i>	<i>69</i>	<i>1.2</i>	<i>58</i>
<i>1225</i>	<i>11</i>	<i>2055</i>	<i>28.9</i>	<i>58</i>	<i>0.9</i>	<i>59</i>

PLANT *Chloron (E-72)*

OPERATOR *Best*

LOCATION *SUS 69 outlet*

DATE *2-8-54*

TIME

INITIAL FINAL
 AMBIENT PRESSURE (IN. HG.) *29.37 29.35*

AMBIENT TEMPERATURE (°F)

SAMPLING POINT *30" above CM*

TEST NUMBER *Run 3*

NO_x SAMPLING DATA

Time	Flask Number	Flask Volume (ml.)	Initial Conditions		Final Conditions	
			Flask Vacuum (in. Hg.)	Flask Temp (°F)	Flask Vacuum (in. Hg.)	Flask Temp (°F)
<i>1155</i>	<i>10</i>	<i>2060</i>	<i>25.9</i>	<i>51</i>	<i>0.4</i>	<i>59</i>
<i>1310</i>	<i>F52</i>	<i>2043</i>	<i>25.7</i>	<i>70</i>	<i>+0.2</i>	<i>60</i>
<i>1320</i>	<i>25</i>	<i>2087</i>	<i>25.7</i>	<i>73</i>	<i>2.2</i>	<i>60</i>

PLANT *Cherem (EER)*

OPERATOR *Best*

LOCATION *Sus 67 outlet*

DATE *2-8-54*

TIME

AMBIENT PRESSURE (IN. HG.) *INIT 29.25 FINAL 29.30*

AMBIENT TEMPERATURE (°F)

SAMPLING POINT *30' above LM*

TEST NUMBER *Run 4*

NO_x SAMPLING DATA

Time	Flask Number	Flask Volume (ml.)	Initial Conditions		Final Conditions	
			Flask Vacuum (in. Hg.)	Flask Temp (°F)	Flask Vacuum (in. Hg.)	Flask Temp (°F)
<i>1355</i>	<i>1</i>	<i>1996</i>	<i>28.7</i>	<i>73</i>	<i>2.1</i>	<i>61</i>
<i>1420</i>	<i>6</i>	<i>2062</i>	<i>28.7</i>	<i>75</i>	<i>1.5</i>	<i>62</i>
<i>1435</i>	<i>93</i>	<i>2053</i>	<i>28.6</i>	<i>73</i>	<i>0.0</i>	<i>61</i>

PLANT *Cherion (EPR)*

OPERATOR

LOCATION *SUS 67 outlet*

DATE *2-8-84*

TIME

MT

IN

AMBIENT PRESSURE (IN. HG.) *27.35*

27.30

AMBIENT TEMPERATURE (°F)

SAMPLING POINT *30" above CM*

TEST NUMBER *Run 5*

NO_x SAMPLING DATA

Time	Flask Number	Flask Volume (ml.)	Initial Conditions		Final Conditions	
			Flask Vacuum (in. Hg.)	Flask Temp (°F)	Flask Vacuum (in. Hg.)	Flask Temp (°F)
<i>1610</i>	<i>23</i>	<i>2037</i>	<i>28.6</i>	<i>70</i>	<i>0.0</i>	<i>61</i>
<i>1635</i>	<i>20</i>	<i>2041</i>	<i>27.2</i>	<i>61</i>	<i>1.1</i>	<i>63</i>
<i>1650</i>	<i>21</i>	<i>2051</i>	<i>28.5</i>	<i>69</i>	<i>2.0</i>	<i>65</i>

PLANT *Chem (EPR)*
LOCATION *SUS-69 outlet*
DATE *2-8-84*

OPERATOR *Best*

TIME
AMBIENT PRESSURE (IN. HG.) *INT 29.30 FIN 29.32*
AMBIENT TEMPERATURE (°F)
SAMPLING POINT *30' above LM*

TEST NUMBER *For 6*

NO_x SAMPLING DATA

Time	Flask Number	Flask Volume (ml.)	Initial Conditions		Final Conditions	
			Flask Vacuum (in. Hg.)	Flask Temp (°F)	Flask Vacuum (in. Hg.)	Flask Temp (°F)
<i>1710</i>	<i>8</i>	<i>1995</i>	<i>28.5</i>	<i>69</i>	<i>1.7</i>	<i>64</i>
<i>1725</i>	<i>7</i>	<i>2046</i>	<i>28.5</i>	<i>69</i>	<i>0.4</i>	<i>64</i>
<i>174</i>	<i>FS1</i>	<i>2053</i>	<i>28.2</i>	<i>69</i>	<i>1.1</i>	<i>66</i>

PLANT *(Levran (EGR))* OPERATOR *Best*
 LOCATION *SPS-69 outlet*
 DATE *2-8-84*
 TIME
 AMBIENT PRESSURE (IN. HG.) *INIT 29.30 FIN 29.32*
 AMBIENT TEMPERATURE (°F)
 SAMPLING POINT *30" above CM*
 TEST NUMBER *Run 7*

NO_x SAMPLING DATA

Time	Flask Number	Flask Volume (ml.)	Initial Conditions		Final Conditions	
			Flask Vacuum (in. Hg.)	Flask Temp (°F)	Flask Vacuum (in. Hg.)	Flask Temp (°F)
<i>1810</i>	<i>5</i>	<i>1989</i>	<i>28.5</i>	<i>68</i>	<i>1.2</i>	<i>65</i>
<i>1825</i>	<i>1</i>	<i>1996</i>	<i>28.6</i>	<i>72</i>	<i>1.6</i>	<i>65</i>
<i>1845</i>	<i>7A</i>		<i>27.3</i>	<i>72</i>	<i>1.3</i>	<i>65</i>

PLANT *Chickens (EGG)* OPERATOR *Best*

LOCATION *SVS 69 outlet*

DATE *2-8-54*

TIME

AMBIENT PRESSURE (IN. HG.) *141T 29.30 121V 29.32*

AMBIENT TEMPERATURE (°F)

SAMPLING POINT *30' above CP*

TEST NUMBER *Run 8*

NO_x SAMPLING DATA

Time	Flask Number	Flask Volume (ml.)	Initial Conditions		Final Conditions	
			Flask Vacuum (in. Hg.)	Flask Temp (°F)	Flask Vacuum (in. Hg.)	Flask Temp (°F)
<i>1910</i>	<i>22</i>	<i>2045</i>	<i>28.2</i>	<i>72</i>	<i>1.1</i>	<i>67</i>
<i>1930</i>	<i>24</i>	<i>2044</i>	<i>28.3</i>	<i>69</i>	<i>0.9</i>	<i>67</i>
<i>1950</i>	<i>19</i>	<i>2064</i>	<i>28.6</i>	<i>67</i>	<i>1.5</i>	<i>67</i>

PLANT *Chem (E212)*

OPERATOR *East*

LOCATION *SUS 69 outlet*

DATE *2-5-84*

TIME

AMBIENT PRESSURE (IN. HG.) *INIT 29.30 FIN 29.32*

AMBIENT TEMPERATURE (°F)

SAMPLING POINT *30" above CM*

TEST NUMBER *Run 9*

NO_x SAMPLING DATA

Time	Flask Number	Flask Volume (ml.)	Initial Conditions		Final Conditions	
			Flask Vacuum (in. Hg.)	Flask Temp (°F)	Flask Vacuum (in. Hg.)	Flask Temp (°F)
<i>2010</i>	<i>18</i>	<i>2079</i>	<i>28.0</i>	<i>65</i>	<i>28.0</i>	<i>67</i>
<i>2025</i>	<i>16</i>	<i>2017</i>	<i>28.6</i>	<i>79</i>	<i>28.0</i>	<i>68</i>
<i>2040</i>	<i>9</i>	<i>2077</i>	<i>28.6</i>	<i>74</i>		

PLANT *Chelon (EER)*

OPERATOR *Best*

LOCATION *Outlet*

DATE *2-24-84*

TIME

AMBIENT PRESSURE (IN. HG.) *INITIAL 29.52 FINAL 29.50*

AMBIENT TEMPERATURE (°F) *65*

SAMPLING POINT *10*

TEST NUMBER *Run 1*

NO_x SAMPLING DATA

Time	Flask Number	Flask Volume (ml.)	Initial Conditions		Final Conditions	
			Flask Vacuum (in. Hg.)	Flask Temp (°F)	Flask Vacuum (in. Hg.)	Flask Temp (°F)
<i>1214</i>	<i>23</i>	<i>2037</i>	<i>29.2</i>	<i>65</i>	<i>0.2</i>	<i>43</i>
<i>1233</i>	<i>10</i>	<i>2060</i>	<i>28.9</i>	<i>69</i>	<i>0.0</i>	<i>43</i>
<i>1249</i>	<i>2</i>	<i>1995</i>	<i>28.9</i>	<i>73</i>	<i>2.8</i>	<i>43</i>

PLANT *Chorron (EER)*OPERATOR *Leit*LOCATION *Outlet*DATE *2-24-84*

TIME

AMBIENT PRESSURE (IN. HG.)

AMBIENT TEMPERATURE (°F)

SAMPLING POINT *10*

	INITIAL	FINAL
AMBIENT PRESSURE (IN. HG.)	<i>29.32</i>	<i>29.50</i>
AMBIENT TEMPERATURE (°F)	<i>65</i>	

TEST NUMBER *run 2*NO_x SAMPLING DATA

Time	Flask Number	Flask Volume (ml.)	Initial Conditions		Final Conditions	
			Flask Vacuum (in. Hg.)	Flask Temp (°F)	Flask Vacuum (in. Hg.)	Flask Temp (°F)
<i>1314</i>	<i>10</i>	<i>2060</i>	<i>29.0</i>	<i>64</i>	<i>3.0</i>	<i>43</i>
<i>1529</i>	<i>43</i>	<i>2053</i>	<i>28.1</i>	<i>73</i>	<i>0.0</i>	<i>43</i>
<i>1546</i>	<i>FS2</i>	<i>2043</i>	<i>29.0</i>	<i>74</i>	<i>1.7</i>	<i>43</i>

PLANT *Chemura (CER)*OPERATOR *Best*LOCATION *Outlet*DATE *2-24-84*

TIME

*INITIAL**FINAL*

AMBIENT PRESSURE (IN. HG.)

*29.32**29.30*

AMBIENT TEMPERATURE (°F)

*65*SAMPLING POINT *10*TEST NUMBER *run 3*NO_x SAMPLING DATA

Time	Flask Number	Flask Volume (ml.)	Initial Conditions		Final Conditions	
			Flask Vacuum (in. Hg.)	Flask Temp (°F)	Flask Vacuum (in. Hg.)	Flask Temp (°F)
<i>1414</i>	<i>2A</i>	<i>2011</i>	<i>28.7</i>	<i>69</i>	<i>3.3</i>	<i>44</i>
<i>1429</i>	<i>7</i>	<i>2046</i>	<i>28.8</i>	<i>71</i>	<i>3.1</i>	<i>45</i>
<i>1445</i>	<i>19</i>	<i>2064</i>	<i>28.9</i>	<i>70</i>	<i>0.4</i>	<i>47</i>

SECTION 5
ANALYTICAL RESULTS

- 5.1 Fuel Proximate and Ultimate Analyses
- 5.2 Particulate and Sulfur Oxides Emissions from Method 5/8 Samples
- 5.3 Particulate Emissions from SASS Samples
- 5.4 Particulate Emissions and Size Distributions from Andersen Samples
- 5.5 Sulfur Oxides Emissions from Controlled Condensation System Samples
- 5.6 Trace Element Analyses of Fuel and SASS Samples
- 5.7 Organic Analyses of SASS Samples: Total Chromatographable Organics (TCO), Gravimetric Organics (GRAV), Gas Chromatography Mass Spectrometry (GC/MS), and Infrared (IR) Spectra of Total Sample Extracts
- 5.8 Volatile Organics Analyses of VOST Traps
- 5.9 N₂O Emissions by GC/ECD
- 5.10 NO_x Emissions by EPA Method 7

5.1 FUEL PROXIMATE AND ULTIMATE ANALYSES

LABORATORY CERTIFICATE

CURTIS & TOMPKINS, LTD.

ESTABLISHED 1878

Bulk Oil & Chemical Surveyors, Samplers & Weighers
Analytical & Consulting Chemists

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ENVIRONMENTAL ANALYSTS
MEMBERS, OFFICIAL CHEMISTS
AND/OR SAMPLERS FOR GOVERNMENT
AGENCIES AND TRADE ORGANIZATIONS

Laboratory No. 84e34
Preliminary No. 7758

Reported 5/3/84
Sampled -----
Received 3/23/84

For ACUREX CORPORATION

Report on 1 sample of Fuel

Mark Sample No. 901440
Subcontract No. RB59186A
Release No. 13
Prime Contract 62-02-3176
Acurex Project No. 7951

ULTIMATE ANALYSIS

Carbon	-----	86.2
Hydrogen	-----	11.3
Oxygen	-----	0.4
Sulfur (1st test)	-----	1.00
Sulfur (2nd test)	-----	1.10
Sulfur (3rd test)	-----	1.08
Nitrogen (1st test)	-----	1.04
Nitrogen (2nd test)	-----	1.09
Nitrogen (3rd test)	-----	1.00

PROXIMATE ANALYSIS

Gross Heating Value, BTU per lb.	-----	18,430
Moisture	-----	0.57
Ash	-----	0.03

Specific Gravity (API)@ +60°F ----- 12.6

Curtis & Tompkins Ltd.

5.2 PARTICULATE AND SULFUR OXIDES EMISSIONS FROM METHOD 5/8 SAMPLES

ISOKINETIC PERFORMANCE WORKSHEET & PARTICULATE CALCULATIONS

Plant CHEU/EEB

Performed by Dr. Ros

Date 2-6-84

Sample Location _____

Test No./Type 1 / M-5/8

Barometric Pressure (in. Hg)	P_b	29.28
Meter volume (std), $17.64 \left(\frac{V_m}{\alpha} \right) \left(\frac{P_b + \frac{\Delta H}{13.6}}{T_m + 460} \right)$ $17.64 \left(\frac{(56.65)}{(1.995)} \right) \left(\frac{(29.28) + \frac{(2.075)}{13.6}}{(69.9) + 460} \right)$	$V_{m \text{ std}}$	55.772
Volume of liquid collected (grams)	V_{l_c}	no data
Volume of liquid at standard condition (scf) $V_{l_c} \times 0.04707$	$V_{w \text{ std}}$	6.047 ✓
Stack gas proportion of water vapor $\frac{V_{w \text{ std}}}{V_{w \text{ std}} + V_{m \text{ std}}}, \frac{(\quad)}{(\quad) + (\quad)}$	B_{wo}	0.0978 From Run 2
Molecular weight, stack gas dry (lb/lb-mole) $(\% \text{ CO}_2 \times 0.44) + (\% \text{ O}_2 \times 0.32) + (\% \text{ N}_2 + \% \text{ CO} \times 0.28)$ $\frac{(14.9 \times 0.44) + (2.9 \times 0.32) + (82.2 + \quad \times 0.28)}{6.556 + .928 + 23.016}$	M_d	30.5 PRELIMINARY DATA
Molecular weight, stack gas wet (lb/lb-mole) $M_d(1-B_{wo}) + 18(B_{wo}), (30.5)(1-.0978) + 18(.0978)$	M_s	29.28 BASED ON PRELIM. DATA
Absolute stack pressure (in. Hg) $P_b + \frac{P_{\text{stack}} (\text{in. H}_2\text{O})}{13.6}, (29.28) + \frac{(+.2)}{13.6}$	P_s	29.29 ✓

✓ BACK CALCULATED BASED ON RUN 2 DATA

7602/5/81/Rev 1

Row 1 / M-5/8

CHEU/EEK

Temperature stack gas, average (°F)	T_s	456.2
Stack velocity (fps) $85.49 (C_p) (\sqrt{\Delta P_{s \text{ avg}}}) \sqrt{\frac{T_{s \text{ avg}} + 460}{P_s M_s}}$ $85.49 (.77) (\sqrt{.649})^2 \sqrt{\frac{(456.2) + 460}{(29.29)(29.29)}}$	$V_{s(\text{avg})}$	45.30
Total sample time (minutes)	θ	72
Nozzle diameter, actual (inches)	N_d	.309
Percent isokinetic (%) $\frac{17.33 (T_s + 460)(V_w \text{ std} + V_m \text{ std})}{\theta V_s P_s N_d^2}$ $\frac{17.33 (456.2 + 460)((.6047) + (.5577))}{(72)(45.30)(29.29)(.309)^2}$	%I	107.6
Area of stack (ft ²) $\pi = 3.1416$ 36" diam $\pi r^2 \div 144, \pi (.18)^2 \div 144$	A_s	7.069
Stack gas volume at standard conditions (dscfm) $60 (1 - B_{wo}) V_{s \text{ avg}} A_s \left(\frac{528}{T_{s \text{ avg}} + 460} \right) \left(\frac{P_s}{29.92} \right)$ $60 (1 - .0778) (45.30) (7.069) \left(\frac{528}{456.2 + 460} \right) \left(\frac{(29.29)}{(29.92)} \right)$	Q_s	7779
Particulate matter concentration, dry (gr/dscf) $15.432 \frac{M_p (\text{grams})}{V_m \text{ std}}, 15.432 \frac{(\quad)}{(\quad)}$	$C_{s(\text{std})}$	
Emission rate of particulate matter (lb/hr) $0.00857 (Q_s) C_{s(\text{std})}, 0.00857 (\quad)(\quad)$	E_p	

2) Assumed

7602/5/81/Rev 1

ISOKINETIC PERFORMANCE WORKSHEET & PARTICULATE CALCULATIONS

Plant CHEU/EEB

Performed by D. Ros

Date 2-6-84

Sample Location OUTLET STACK

Test No./Type 2 / M-S18

Barometric Pressure (in. Hg)	P_b	29.28
Meter volume (std), $17.64 \left(\frac{V_m}{\alpha} \right) \left(\frac{P_b + \frac{\Delta H}{13.6}}{T_m + 460} \right)$ $17.64 \left(\frac{57.943}{(1.995)} \right) \left(\frac{(29.28) + \frac{(2.18)}{13.6}}{(77.8) + 460} \right)$	$V_{m \text{ std}}$	56.223
Volume of liquid collected (grams)	V_{l_c}	129.5
Volume of liquid at standard condition (scf) $V_{l_c} \times 0.04707$	$V_{w \text{ std}}$	6.096
Stack gas proportion of water vapor $\frac{V_{w \text{ std}}}{V_{w \text{ std}} + V_{m \text{ std}}}, \frac{(6.096)}{(6.096) + (56.223)}$	B_{wo}	0.0978
Molecular weight, stack gas dry (lb/lb-mole) $(\% \text{ CO}_2 \times 0.44) + (\% \text{ O}_2 \times 0.32) + (\% \text{ N}_2 + \% \text{ CO} \times 0.28)$ $(\text{ } \times 0.44) + (\text{ } \times 0.32) + (\text{ } + \text{ } \times 0.28)$	M_d	30.5 PRELIMINARY DATA (SEE RUN 1)
Molecular weight, stack gas wet (lb/lb-mole) $M_d(1-B_{wo}) + 18(B_{wo}), (\text{ })(1-\text{ }) + 18(\text{ })$	M_s	29.28 BASED ON PRELIM. DATA (SEE RUN 1)
Absolute stack pressure (in. Hg) $P_b + \frac{P_{\text{stack}} (\text{in. H}_2\text{O})}{13.6}, (29.28) + \frac{(0.2)}{13.6}$	P_s	29.29

7602/5/81/Rev 1

Temperature stack gas, average (°F)	T_s	479.1
Stack velocity (fps) $85.49 (C_p) (\sqrt{\Delta P_s \text{ avg}}) \sqrt{\frac{T_{s \text{ avg}} + 460}{P_s M_s}}$ $85.49 (.79) (\sqrt{.6696})^2 \sqrt{\frac{(479.1) + 460}{(29.21)(29.25)}}$	$V_{s(\text{avg})}$	47.32
Total sample time (minutes)	θ	72
Nozzle diameter, actual (inches)	N_d	.309
Percent isokinetic (%) $17.33 (T_s + 460)(V_w \text{ std} + V_m \text{ std})$ $\frac{\theta V_s P_s N_d^2}{17.33 (479.1 + 460)((.096) + (.222))}$ $\frac{(72)(47.32)(29.29)(.309)^2}{(72)(47.32)(29.29)(.309)^2}$	%I	106.44
Area of stack (ft ²) $\pi = 3.1416$ $\pi r^2 \div 144, \quad \pi (.18)^2 \div 144$	A_s	7.069
Stack gas volume at standard conditions (dscfm) $60 (1 - B_{wo}) V_{s \text{ avg}} A_s \left(\frac{528}{T_s \text{ avg} + 460} \right) \left(\frac{P_s}{29.92} \right)$ $60 (1 - .0174) (47.32) (7.069) \left(\frac{528}{479.1 + 460} \right) \left(\frac{29.21}{29.92} \right)$	Q_s	9966
Particulate matter concentration, dry (gr/dscf) $15.432 \frac{M_p (\text{grams})}{V_m \text{ std}}, \quad 15.432 \frac{(\quad)}{(\quad)}$	$C_{s(\text{std})}$	
Emission rate of particulate matter (lb/hr) $0.00857 (Q_s) C_{s(\text{std})}, \quad 0.00857 (\quad)(\quad)$	E_p	

Assumed

ACUREX ANALYTICAL REPORT

Sample of: CMEA

Sample Date: 2-1-84

Requested By: LARRY WATERLAND, PLD

I.D. Number: 307735-81

Analytical Method: Gravimetric Analyses of EPA 5/8 Front Filters & Probe Washes

Date of Analysis: 2-9-84

Filter # or TOTAL VOL. ACETONE FINAL - TARE = NET WT			
Lab I.D. Number	Component	Analytical Result	Unit
901479 (Filter Blank)	84-95.3-001	0.47822 - 0.47824 = -0.00002 g	grams of Particulate ↓
901467 (Filter, Run#1)	84-953-010	0.57543 - 0.48021 = 0.09522 g	
901471 (Filter, Run#2)	84-95.3-008	0.59386 - 0.47772 = 0.11614 g	
901478 (ACETONE BLANK)	450 MLS	1.46443 - 1.46365 = 0.00078 g / 450 mls = 1.73333 x 10 ⁻⁶ g/mL ACE.	
901446 (Probe Wash, Run#1)	126 mls	1.47268 - 1.46736 = 0.00532	
901468 (Probe Wash, Run#2)	176 mls	1.55260 - 1.47117 = 0.08743 g	
NB.: ALL REPORTED VALUES HAVE <u>NOT</u> Been corrected for Blanks.			

Analysis By Martin M. Murray

5-9

Date 3-12-84

ACUREX ANALYTICAL REPORT

Sample of: CMFA/ERR

Sample Date: 2-1-84

Requested By: L. Waterland

I.D. Number: 307735.81

Analytical Method: Gravimetric Analysis of Method 5/8 Condensibles

Date of Analysis: 3/3 - 3/16/84

TOTAL Volume/
Aliquot

Lab I.D. Number	Component	Analytical Result	Unit
901447 Run #1	224/50	0.13700	grams ↓
	224/50	0.13422	
901469 Run #2	257/50	0.02631	
	257/50	0.02092	
901466 IPA Blank	50 mls	0.00041	
N.B. All samples were analyzed in duplicate and the results reported <u>have</u> <u>been</u> blank corrected			

Analysis By Martha M. Murray

5-10 Date 3-16-84

ACUREX ANALYTICAL REPORT

Sample of: CMEA

Sample Date: 2-1-84

Requested By: LARRY WATERLAND

I.D. Number: 307735.81

Analytical Method: SULFATE TITRATIONS OF EPA 5/8 IMPINGER CATCHES

Date of Analysis: 2-6-84

TOTAL VOL/BLK			
Lab I.D. Number	Component	Analytical Result	Unit
901447 (Imp. #1 + Filter, TEST #1)	$\frac{174 \text{ mL}}{25 \text{ mL}}$	82.72	TOTAL mg Sulfate per sample ↓
901450 + 901452 (Imp. 2+3, TEST #1)	$\frac{338 \text{ mL}}{5/100 \times 10 \text{ mL}}$	3968.4	
901469 (Imp. #1 + FILTER, TEST #2)	$\frac{207 \text{ mL}}{25 \text{ mL}}$	28.33	
901472 (Imp. #2 + 3, TEST #2)	$\frac{362 \text{ mL}}{5/100 \times 10 \text{ mL}}$	3,833 (100.1% recovery on spike)	
901466 (80% IPA + Filter BLANK)	$\frac{328 \text{ mL}}{25 \text{ mL}}$	0.00 (INSTANT ENDPOINT)	
901465 (6% H ₂ O ₂ BLANK)	$\frac{196 \text{ mL}}{10 \text{ mL}}$	0.00 (INSTANT ENDPOINT)	
* EPA STANDARDS (SUBMITTED BY B. DAROS)			mg/DSCM ↓
#2A (Lot 0881 #233)	$\frac{100 \text{ mL}}{10 \text{ mL}}$	1294.9	
#3A (Lot 0881 #333)	$\frac{100 \text{ mL}}{10 \text{ mL}}$	200.7	
STANDARDIZATION OF BaCl ₂ · 2H ₂ O: 2-6-84: V ₂ = 10 mL; N ₂ = 0.01; V ₁ = 9.98, 10.03 (10.01 mL AVERAGE); N ₁ = 0.0100 N			

* True Value = 1296.4 mg/dscm
xx " = 190.7 mg/dscm

5-11

Analysis By Maria M. Murray

Date 3-13-84

5.3 PARTICULATE EMISSIONS FROM SASS SAMPLES

ISOKINETIC PERFORMANCE WORKSHEET & PARTICULATE CALCULATIONS

Plant CHEVRON UTA / EENE LINDEN Performed by Robert
 Date 12-5-84
 Sample Location Steam Outlet
 Test No./Type SASS

Barometric Pressure (in. Hg)	P_b	
Meter volume (std), $17.64 \left(\frac{V_m}{\alpha} \right) \left(\frac{P_b + \frac{\Delta H}{13.6}}{T_m + 460} \right)$ $17.64 \left(\frac{(866.4)}{(1.039)} \right) \left(\frac{(29.9)}{(95)} + \frac{(1.9)}{460} \right)$	$V_{m \text{ std}}$	796
Volume of liquid collected (grams)	V_{l_c}	1920
Volume of liquid at standard condition (scf) $V_{l_c} \times 0.04707$	$V_{w \text{ std}}$	90.37
Stack gas proportion of water vapor $\frac{V_{w \text{ std}}}{V_{w \text{ std}} + V_{m \text{ std}}}, \frac{(90.37)}{(796) + (90.37)}$	B_{wo}	0.103
Molecular weight, stack gas dry (lb/lb-mole) $(\% \text{ CO}_2 \times 0.44) + (\% \text{ O}_2 \times 0.32) + (\% \text{ N}_2 + \% \text{ CO} \times 0.28)$ $(13.1 \times 0.44) + (2.7 \times 0.32) + (84.2 + \text{ } \times 0.28)$	M_d	30.2
Molecular weight, stack gas wet (lb/lb-mole) $M_d(1-B_{wo}) + 18(B_{wo}), (30.2)(1-0.103) + 18(0.103)$	M_s	29.9
Absolute stack pressure (in. Hg) $P_b + \frac{P_{\text{stack}} (\text{in. H}_2\text{O})}{13.6}, (29.3) + \frac{(\text{ })}{13.6}$	P_s	29.3

Form 440 3/84

Temperature stack gas, average (°F)	T_s	456
Stack velocity (fps) $85.49 (C_p) (\sqrt{\Delta P_s \text{ avg}}) \sqrt{\frac{T_s \text{ avg} + 460}{P_s M_s}}$ $85.49 (0.616) (\sqrt{0.632}) \sqrt{\frac{(456) + 460}{(29.3)(29.3)}}$	$V_{s(\text{avg})}$	45.3
Total sample time (minutes)	θ	240
Nozzle diameter, actual (inches)	N_d	0.674
Percent isokinetic (%) $\frac{17.33 (T_s + 460)(V_w \text{ std} + V_m \text{ std})}{\theta V_s P_s N_d^2}$ $\frac{17.33 (456 + 460)((70.4) + (72.6))}{(240)(45.3)(29.3)(0.674)^2}$	%I	96.2
Area of stack (ft ²) $\pi = 3.1416$ $\pi r^2 \div 144, \pi (\text{_____})^2 \div 144$	A_s	7.069
Stack gas volume at standard conditions (dscfm) $60 (1 - B_{wo}) V_{s \text{ avg}} A_s \left(\frac{528}{T_s \text{ avg} + 460} \right) \left(\frac{P_s}{29.92} \right)$ $60 (1 - 0.103)(45.3)(7.069) \left(\frac{528}{456 + 460} \right) \left(\frac{29.3}{29.92} \right)$	Q_s	9836
Particulate matter concentration, dry (gr/dscf) $15.432 \frac{M_p(\text{grams})}{V_m \text{ std}}, 15.432 \frac{(\text{_____})}{(\text{_____})}$	$C_{s(\text{std})}$	
Emission rate of particulate matter (lb/hr) $0.00857 (Q_s) C_{s(\text{std})}, 0.00857 (\text{_____})(\text{_____})$	E_p	

Plant EPA Sample No. —
Sampling Location Chevron EER Run No. 1
Recovered By C. Beeman Recovery Date 2-1-84 Run Date 2-1-84
Comments _____
Analyst Responsible _____
Calculations and Report Reviewed By _____ Report Date _____

FILTERS USED		CYCLONES	
No.		Used (yes/no)	Pretared Container (No.)
		10μ	
		3μ	
		1μ	

IMPINGER VOLUMES			
	Initial		Final
First (H ₂ O ₂)	500 ml	}	547 ml
Second (APS + AgNO ₃)	500 ml		840 ml
Third (APS + AgNO ₃)	500 ml		ml
TOTALS	1500 ml		ml

53 ml rise

100 ml. rise

Gain _____ ml

SILICA GEL WEIGHTS		
Initial	Final	
1089.8 g	1322.6 g	silica gel totally spent
973.7 g	1115.2 g	
_____ g	_____ g	
TOTALS _____ g	_____ g	Gain _____

CONDENSATE		1920 ml
TOTAL VOLUME COLLECTED		
Volume Neat	1920 ml	
Volume Extracted	_____ ml	Ph-13
Volume CH ₂ Cl ₂ Extract (3 x _____ ml)	_____ ml	
Extracted Condensate:		
pH Neat	_____	
Amount 96% HNO ₃ added	_____	
pH Final	_____	
TOTAL GAIN		_____ ml

Note: Imp. solutions and combinations were bubbling

ACUREX ANALYTICAL REPORT

Sample of: CMEA / EER

Sample Date: 2-1-84

Requested By: L. Waterland

I.D. Number: 307735.81

Analytical Method: Gravimetric Analyses of SASS Filters and probe wash

Date of Analysis: 2/9 ~ 3/13/84

Date of Analysis: 1/11/2017		Filter # or Volume	
Lab I.D. Number	Component	Analytical Result	Unit
901460 (probe/nozzle rinse)	117 mls	0.05014	grams ↓ V
901481 (meCl ₂ blank)	50 mls	-0.00008	
901458	84-142-034	0.12175	
901459 (Filter Blank)	84-142-035	0.00005	
901457	84-142-033	0.12797	
901456	84-142-032	0.15379	
901455	84-142-031	0.11046	
NB: ALL RESULTS HAVE BEEN BLANK CORRECTED			

Analysis By Mark M. Murray

5-16 Date 3-16-84

5.4 PARTICULATE EMISSIONS AND SIZE DISTRIBUTIONS FROM ANDERSEN SAMPLES

PARTICULATE CALCULATIONS

55R
Andersen #1
2-22-84

1. Volume of dry gas sampled at standard conditions, 68°F, 29.92 inch Hg (scf)

$$V_{m_{std}} = 17.64 \frac{V_m}{\alpha} \left(\frac{P_b + \frac{\Delta H}{13.6}}{T_{m,avg} + 460} \right) = 17.64 \frac{14.982}{1.001} \left(\frac{29.36 + \frac{0.9}{13.6}}{65.2 + 460} \right) = 14.793$$

$$\text{or } V_{m_{stack}} = \left(\frac{V_m}{\alpha(1 - B_{wo})} \right) \left(\frac{T_{s,avg} + 460}{T_{m,avg} + 460} \right) \left(\frac{P_m}{P_s} \right) \quad (\text{act at stack conditions})$$

2. Stack gas moisture condensed at standard conditions (scf)

$$V_{w_{std}} = 0.04707 V_{I_c} = \frac{V_{m_{std}}(B_{wo})}{1 - B_{wo}} = 1.941$$

3. Stack gas proportion of water vapor, by volume

$$B_{wo} = \frac{V_{w_{std}}}{V_{w_{std}} + V_{m_{std}}} = 11.60\%$$

4. Stack gas dry molecular weight (lb/lb-mole)

$$MW_d = 0.44 \left(\frac{13.0}{100} \right) + 0.32 \left(\frac{3.0}{100} \right) + 0.28 \left(\frac{84.0}{100} \right) = 30.20$$

5. Stack gas molecular weight (lb/lb-mole)

$$MW_s = MW_d (1 - B_{wo}) + 18 (B_{wo}) = 28.78$$

6. Pressure stack, in. Hg

$$P_s = P_b + \frac{P_{st}}{13.6} = 29.36 + \frac{-0.25}{13.6} = 29.34$$

7. Stack gas velocity at stack conditions (ft/sec)

$$V_s = 85.49 (C_p) (\sqrt{\Delta P})_{avg} \sqrt{\frac{T_{s,avg} + 460}{P_s MW_s}}$$

$$= 85.49 (1.84) (0.663) \sqrt{\frac{531.5 + 460}{(29.30)(59.3)}} = 50.267$$

8. Stack gas volume at standard conditions (scfm)

$$Q_s = 60 (1 - B_{wo}) V_{s,avg} A_s \left(\frac{528}{T_{s,avg} + 460} \right) \left(\frac{P_s}{29.92} \right)$$

$$\text{or } Q_a = 60 V_{s,avg} A_s \text{ (acfm) =}$$

9. Test percent isokinetic

$$\%I = \frac{17.33(T_{s,avg} + 460) [V_{w,std} + V_{m,std}]}{\theta V_s P_s D_n^2} = \frac{17.33(T_s + 460)(V_{m,std})}{\theta V_s P_s D_n^2 (1 - B_{wo})}$$

$$\frac{17.33(991.5)(16.590)}{(30.2)(50.267)(29.30)(.250)} = 102.91\%$$

10. Particulate matter concentration, gr/scf

$$C_s = 15.432 \frac{M_p}{V_{m,std}} = 0.0167$$

$$\text{or } C_a = 15.432 \frac{M_p}{V_{m,stack}} \text{ (gr/acf) =}$$

11. Emission rate of particulate matter, lb/hr

$$ER = 0.00857 (Q_s) C_s$$

=

12. Percent excess air at sampling point

$$\% EA = \frac{100 [\%O_2 - 0.5 (\%CO)]}{0.264 \%N_2 - (\%O_2 - 0.5 \times \%CO)} =$$

13. Emission rate of particulate matter, lb/10⁶ Btu

$$E = 2.679 \times 10^6 \left(\frac{M_p}{V_{m,std}} \right) F \left(\frac{20.9}{20.9 - \%O_2} \right)$$

=

PARTICULATE CALCULATIONS

EEA
Answer #2
2-22-84

1. Volume of dry gas sampled at standard conditions, 68° F, 29.92 inch Hg (scf)

$$V_{m_{std}} = 17.64 \frac{V_m}{\alpha} \left(\frac{P_b + \frac{\Delta H}{13.6}}{T_{m,avg} + 460} \right) = 17.64 \frac{14.676}{1.001} \left(\frac{29.32 + \frac{0.7}{13.6}}{59.8 + 460} \right) = 14.621$$

$$\text{or } V_{m_{stack}} = \left(\frac{V_m}{\alpha(1 - B_{wo})} \right) \left(\frac{T_{s,avg} + 460}{T_{m,avg} + 460} \right) \left(\frac{P_m}{P_s} \right) \quad (\text{acf at stack conditions})$$

2. Stack gas moisture condensed at standard conditions (scf)

$$V_{w_{std}} = 0.04707 V_{I_c} = \frac{V_{m_{std}}(B_{wo})}{1 - B_{wo}} = 1.919$$

3. Stack gas proportion of water vapor, by volume

$$B_{wo} = \frac{V_{w_{std}}}{V_{w_{std}} + V_{m_{std}}} = 11.60\%$$

4. Stack gas dry molecular weight (lb/lb-mole)

$$MW_d = 0.44 (\%CO_2) + 0.32 (\%O_2) + 0.28 (\%N_2 + \%CO) = 30.36$$

5. Stack gas molecular weight (lb/lb-mole)

$$MW_s = MW_d (1 - B_{wo}) + 18 (B_{wo}) = 28.93$$

6. Pressure stack, in. Hg

$$P_s = P_b + \frac{P_{st}}{13.6} = 29.32 + \frac{-0.25}{13.6} = 29.30$$

7. Stack gas velocity at stack conditions (ft/sec)

$$V_s = 85.49 (C_p) (\sqrt{\Delta P})_{avg} \sqrt{\frac{T_{s,avg} + 460}{P_s MW_s}}$$

$$\underline{85.49 (0.82) (0.663) \sqrt{\frac{552.5 + 460}{(27.34)(28.78)}}} = 50.894$$

8. Stack gas volume at standard conditions (scfm)

$$Q_s = 60 (1 - B_{wo}) V_{s,avg} A_s \left(\frac{528}{T_{s,avg} + 460} \right) \left(\frac{P_s}{29.92} \right)$$

$$\text{or } Q_a = 60 V_{s,avg} A_s \text{ (acfm) =}$$

9. Test percent isokinetic

$$\%I = \frac{17.33(T_{s,avg} + 460) [V_{w,std} + V_{m,std}]}{\theta V_s P_s D_n^2} = \frac{17.33(T_s + 460)(V_{m,std})}{\theta V_s P_s D_n^2 (1 - B_{wo})}$$

$$= \frac{17.33(1012.5)(16.734)}{(30.15)(50.894)(27.34)(0.250)^2} = 104.35 \%$$

10. Particulate matter concentration, gr/scf

$$C_s = 15.432 \frac{M_p}{V_{m,std}} = 0.0134$$

$$\text{or } C_a = 15.432 \frac{M_p}{V_{m,stack}} \text{ (gr/acf) =}$$

11. Emission rate of particulate matter, lb/hr

$$ER = 0.00857 (Q_s) C_s$$

12. Percent excess air at sampling point

$$\% EA = \frac{100 [\%O_2 - 0.5 (\%CO)]}{0.264 \%N_2 - (\%O_2 - 0.5 \times \%CO)} =$$

13. Emission rate of particulate matter, lb/10⁶ Btu

$$E = 2.679 \times 10^6 \left(\frac{M_p}{V_{m,std}} \right) F \left(\frac{20.9}{20.9 - \%O_2} \right)$$

ANDERSEN PARTICLE SIZE ANALYSIS

Plant CHEVRON SRS-69
 Test Location SRS-69 Outlet
 Run No. 1
 Flow Rate 1.08 ACFM

Tare Weights:
 Date 2/13/80
 By K. BREWSTER
 Location MT View

Final Weights:
 Date 2/15/80
 By K. BREWSTER
 Location MT View

STAGE NO.	FILTER NO.	FINAL WT (g)	TARE WT (g)	SAMPLE WT (g) ^a	% OF TOTAL WT ^b	CUMULATIVE % OF TOTAL WT ^b	Dp μ
0	UOP-23-1	1.23277	1.23293	0		100.00	7.52
1	UOP-23-2	1.23529	1.21493	0.00020	1.55	98.45	7.11
2	UOP-23-3	1.21700	1.21627	0.00057	4.42	94.03	4.35
3	UOP-23-4	1.21362	1.21319	0.00027	2.09	91.94	3.03
4	UOP-23-5	1.21782	1.21744	0.00022	1.71	90.23	1.57
5	UOP-23-6	1.20114	1.20039	0.00059	4.58	85.65	.78
6	UOP-23-7	1.22987	1.22893	0.00078	6.05	79.60	.48
7	UOP-23-8	1.20792	1.20685	0.00071	7.06	72.54	.22
F	UOP-23-F	1.28680	1.27712	0.00935	72.54		

TOTAL WITH FILTER 12.89mg
 TOTAL WITHOUT FILTER 3.54mg

Blank correction value -0.00016 Stages 0 through 7

Blank correction value -0.00033 Stage F (final filter)

^aIncludes appropriate blank correction factor.

^bCalculations based on total sample weight with filter are entered on first line; calculations based on total sample weight without filter are entered on second line for each stage.

Comments: Cyclone rinse = 0 mg

13.04 μ m D₅₀

ANDERSEN PARTICLE SIZE ANALYSIS

Plant CHEVRON SVS-69
 Test Location SVS-69 Outlet
 Run No. 2
 Flow Rate 1.05 ACFM

Tare Weights:
 Date 2/13/84
 By K. BREWSTER
 Location MT VIEW

Final Weights:
 Date 3/5/84
 By K. BREWSTER
 Location MT VIEW

STAGE NO.	FILTER NO.	FINAL WT (g)	TARE WT (g)	SAMPLE WT (g) ^a	% OF TOTAL WT ^b	CUMULATIVE % OF TOTAL WT ^b	Dp μ
0	UOP-20-1	1,24019	1,23960	0.00043	2.72	89.63	7.55
1	UOP-20-2	1,21855	1,21781	0.00058	3.67	85.96	7.15
2	UOP-20-3	1,23509	1,23447	0.00046	2.91	83.05	4.37
3	UOP-20-4	1,21236	1,21164	0.00056	3.54	79.51	3.04
4	UOP-20-5	1,23021	1,22926	0.00079	5.00	74.51	1.58
5	UOP-20-6	1,21475	1,21369	0.00090	5.69	68.82	.79
6	UOP-20-7	1,23182	1,23090	0.00076	4.81	64.01	.49
7	UOP-20-8	1,21294	1,21169	0.00107	6.89	57.12	.22
F	UOP-20F	1,29128	1,28192	0.00903	57.12		

TOTAL WITH FILTER 15.81mg
 TOTAL WITHOUT FILTER 6.78mg

Blank correction value -0.00016 Stages 0 through 7
 Blank correction value -0.00033 Stage F (final filter)

^aIncludes appropriate blank correction factor.

^bCalculations based on total sample weight with filter are entered on first line; calculations based on total sample weight without filter are entered on second line for each stage.

Comments: Cyclone rinse = 1.21mg 7.65% (92.35cum%)
12.52 Pp50

ANDERSEN PARTICLE SIZE ANALYSIS

Plant CHEVRON SLS-69
 Test Location BLANK
 Run No. _____
 Flow Rate _____

Tare Weights:
 Date 2/13/84
 By K. BREWSTER
 Location MT VIEW

Final Weights:
 Date 3/5/84
 By K. BREWSTER
 Location MT VIEW

STAGE NO.	FILTER NO.	FINAL WT (g)	TARE WT (g)	SAMPLE WT (g) ^a	% OF TOTAL WT ^b	CUMULATIVE % OF TOTAL WT ^b	Dp μ
0	UOP-24-1	1.22138	1.22080	.00058			
1	UOP-24-2	1.21042	1.21021	.00021			
2	UOP-24-3	1.22256	1.22249	.00007			
3	UOP-24-4	1.20185	1.20186	-.00001			
4	UOP-24-5	1.22539	1.22535	.00004			
5	UOP-24-6	1.20843	1.20817	.00026			
6	UOP-24-7	1.23253	1.23248	.00005			
7	UOP-24-8	1.21429	1.21420	.00009			
F	UOP-24-F	1.27939	1.27906	.00033			
TOTAL WITH FILTER							
TOTAL WITHOUT FILTER							

Blank correction value = _____ Stages 0 through 7

Blank correction value = 0.00 Stage F (final filter)

^aIncludes appropriate blank correction factor.

^bCalculations based on total sample weight with filter are entered on first line; calculations based on total sample weight without filter are entered on second line for each stage.

Comments:

ACUREX ANALYTICAL REPORT

Sample of: Cherron SVS-69 (EPA)

Sample Date: 2-22-84

Requested By: Regan Best

I.D. Number: _____

Analytical Method: Gravimetric analysis of Anderson cyclone rinses

Date of Analysis: 3-7-84

Lab I.D. Number		Component	Analytical Result	Unit
902226	tin # 186	particulate	10.12	mg
Blank				
* 902229	tin # 184		0.00	
Test 1				
* 902230	tin # 185		+ 1.21	
Test 2				

* these weights are
blank - corrected.

Analysis By [Signature]

5-25 Date 3-8-84

5.5 SULFUR OXIDES EMISSIONS FROM CONTROLLED CONDENSATION SYSTEM SAMPLES

ISOKINETIC PERFORMANCE WORKSHEET & PARTICULATE CALCULATIONS

 Plant Chesam CERR

 Performed by Best

 Date 2-23-87

 Sample Location S/S-69 Outlet

 Test No./Type CCS-1

Barometric Pressure (in. Hg)	P_b	29.34
Meter volume (std), $17.64 \left(\frac{V_m}{\alpha} \right) \left(\frac{P_b + \frac{\Delta H}{13.6}}{T_m + 460} \right)$ $17.64 \left(\frac{22.715}{1.00} \right) \left(\frac{29.34 + \frac{0.4}{13.6}}{62.2 + 460} \right)$	$V_{m \text{ std}}$	20.357
Volume of liquid collected (grams)	V_{l_c}	61
Volume of liquid at standard condition (scf) $V_{l_c} \times 0.04707$	$V_{w \text{ std}}$	2.87
Stack gas proportion of water vapor $\frac{V_{w \text{ std}}}{V_{w \text{ std}} + V_{m \text{ std}}}, \frac{2.87}{2.87 + 20.357}$	B_{wo}	12.4
Molecular weight, stack gas dry (lb/lb-mole) $(\% \text{ CO}_2 \times 0.44) + (\% \text{ O}_2 \times 0.32) + (\% \text{ N}_2 + \% \text{ CO} \times 0.28)$ $(\text{ } \times 0.44) + (\text{ } \times 0.32) + (\text{ } + \text{ } \times 0.28)$	M_d	
Molecular weight, stack gas wet (lb/lb-mole) $M_d(1-B_{wo}) + 18(B_{wo}), (\text{ })(1-\text{ }) + 18(\text{ })$	M_s	
Absolute stack pressure (in. Hg) $P_b + \frac{P_{\text{stack}} (\text{in. H}_2\text{O})}{13.6}, (\text{ }) + \frac{(\text{ })}{13.6}$	P_s	

ISOKINETIC PERFORMANCE WORKSHEET & PARTICULATE CALCULATIONS

 Plant Chen (EER)

 Performed by Bert

 Date 2-23-84

 Sample Location S/S - 69 (Outlet)

 Test No./Type CCS - 2

Barometric Pressure (in. Hg)	P_b	29.32
Meter volume (std), $17.64 \left(\frac{V_m}{\alpha} \right) \left(\frac{P_b + \frac{\Delta H}{13.6}}{T_m + 460} \right)$ $17.64 \left(\frac{20.765}{1.00} \right) \left(\frac{29.32 + \frac{0.4}{13.6}}{61.7 + 460} \right)$	$V_{m \text{ std}}$	20.765
Volume of liquid collected (grams)	V_{l_c}	60.
Volume of liquid at standard condition (scf) $V_{l_c} \times 0.04707$	$V_{w \text{ std}}$	2.82
Stack gas proportion of water vapor $\frac{V_{w \text{ std}}}{V_{w \text{ std}} + V_{m \text{ std}}}, \frac{2.82}{2.82 + 20.765}$	B_{wo}	12.0
Molecular weight, stack gas dry (lb/lb-mole) $(\% \text{ CO}_2 \times 0.44) + (\% \text{ O}_2 \times 0.32) + (\% \text{ N}_2 + \% \text{ CO} \times 0.28)$ $(\text{ } \times 0.44) + (\text{ } \times 0.32) + (\text{ } + \text{ } \times 0.28)$	M_d	
Molecular weight, stack gas wet (lb/lb-mole) $M_d(1-B_{wo}) + 18(B_{wo}), (\text{ })(1-\text{ }) + 18(\text{ })$	M_s	
Absolute stack pressure (in. Hg) $P_b + \frac{P_{\text{stack}} (\text{in. H}_2\text{O})}{13.6}, (\text{ }) + \frac{(\text{ })}{13.6}$	P_s	

ACUREX ANALYTICAL REPORT

Sample of: CMEA/EER

Sample Date: 2-23-84

Requested By: Waterland

I.D. Number: 307735-81

Analytical Method: Sulfate titrations of CCS Samples

Date of Analysis: 3-29-84

Lab I.D. Number	Component	Analytical Result	Unit
902296, 902292, 902295	Run 1 probe, filter, coil rinse	109.1	mg SO ₂ per sample ↓
902291	H ₂ O ₂ impinger Run 1	1382.4	
902302, 902297, 902293	Run 2 probe, filter, coil rinse	119.2	
902300	Run 2 H ₂ O ₂ impinger	1434.7	
902301	D.I. blank	0.0	
902298	H ₂ O ₂ blank	0.0	

Analysis By: Best

5-29 Date: 3-29-84

5.6 TRACE ELEMENT ANALYSES OF FUEL AND SASS SAMPLES

In the following, samples labeled fuel, test 1 and fuel, test 2 are blind duplicate samples of the same material.

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 1919 SOUTH HIGHLAND AVE., SUITE 210-B, LOMBARD, ILLINOIS 60148 • (312) 953-9300

ROBERT L. TAYLOR, Ph.D.
MANAGER
INSTRUMENTAL ANALYSIS DIVISION



PLEASE ADDRESS ALL CORRESPONDENCE TO:
490 ORCHARD ST., GOLDEN, CO 80401
OFFICE TEL. (303) 278-9521

May 16, 1984

Mr. Christopher Mann
Acurex Corporation
P.O. Box 7555
Mountain View, CA 94042

RE: IAD #97-P137-116-10
Subcontract #SW59159A
Release #15

Analytical Report

Ten samples were received for analysis on April 2, 1984. These samples were assigned our IAD identification #97-P137-116-10.

Trace element determinations using Spark Source Mass Spectrometry per EPA level 1 protocol are reported in separate attached reports.

Arsenic and Antimony were determined on two of the samples using hydride generation atomic absorption spectrophotometry. Mercury was determined on all ten samples using flameless cold vapor atomic absorption spectrophotometry. The results of these determinations are presented in Table No. I and are reported in parts per million (ppm) by weight on an "as received" basis.

Carbon and Hydrogen were determined on four samples by an external laboratory. The results of these determinations are presented in Table No. II and are reported in weight percent (Wt.%) on an "as received" basis.



Charter Member

Table No. I
(ppm by Wt.)

<u>Sample ID</u>	<u>Arsenic (As)</u>	<u>Antimony (Sb)</u>	<u>Mercury (Hg)</u>
901458 EOR Filter	--	--	0.04 *
901459 EOR Filter Blank	--	--	≤0.02 *
901454 EOR XAD-2	--	--	0.52
901475 EOR XAD-2 Blank	--	--	≤0.4
901463 EOR Impinger 1	--	--	0.0031
901461 EOR Impinger 1 Blank	--	--	0.0089
901440 EOR Fuel, Test 1	--	--	≤0.4
901441 EOR Fuel, Test 2	--	--	≤0.4
901464 EOR Impinger 2 and 3	0.012	≤0.004	0.004
901462 EOR Impinger 2 & 3 Blank	0.005	≤0.004	≤0.002

* Reported in ppm by weight of the filter.

Table No. II
(Wt.-%As Received)

<u>Sample ID</u>	<u>Carbon</u>	<u>Hydrogen</u>
901458 EOR Filter	0.14 **	0.17 **
901459 EOR Filter Blank	0.05 **	0.02 **
901440 EOR Fuel, Test 1	85.67	11.22
901441 EOR Fuel, Test 2	85.91	11.36

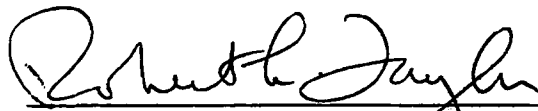
** Reported in weight per cent of the filter.

If you have any questions concerning these results, please call.



Harold A. Connell
Assistant Laboratory Manager

HAC/gh



Robert L. Taylor, Ph.D., Manager
Instrumental Analysis Division

10/24/84

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GENERAL OFFICES: 1919 SOUTH HIGHLAND AVE., SUITE 210-B, LOMBARD, ILLINOIS 60148 AREA CODE 312 953-9300
INSTRUMENTAL ANALYSIS DIVISION, 490 ORCHARD STREET, GOLDEN, COLORADO 80401, PHONE: 303 278-9521

Reply to



To: Acurex Corporation
555 Clyde Avenue
P.O. Box 7555
Mountain View, CA 94039

Date: May 16, 1984

Analyst: G. Meagher

P. O. No.: Subcontract SW59159A, Release # 15, Project #EE7734.82

Sample No.: 901440
EOR Fuel
Test 1

SPARK SOURCE MASS SPECTROGRAPHIC ANALYSIS
CONCENTRATION IN PPM WEIGHT

IAD No.: 97-P137-116-70

ELEMENT	CONC.	ELEMENT	CONC.	ELEMENT	CONC.	ELEMENT	CONC.
Uranium		Terbium		Ruthenium		Vanadium	6
Thorium		Gadolinium		Molybdenum	*2	Titanium	3
Bismuth		Europium		Niobium	0.09	Scandium	≤0.09
Lead	0.6	Samarium		Zirconium	0.2	Calcium	13
Thallium		Neodymium		Yttrium	0.06	Potassium	5
Mercury	NR	Praseodymium		Strontium	0.2	Chlorine	*MC
Gold		Cerium		Rubidium	0.02	Sulfur	MC
Platinum	**1	Lanthanum		Bromine	0.2	Phosphorus	4
Iridium		Barium	0.8	Selenium	0.5	Silicon	19
Osmium		Cesium		Arsenic	0.06	Aluminum	9
Rhenium		Iodine	0.5	Germanium		Magnesium	8
Tungsten		Tellurium		Gallium	0.2	Sodium	10
Tantalum		Antimony		Zinc	2	Fluorine	≈27
Hafnium		Tin		Copper	0.7	Oxygen	NR
Lutetium		Indium	STD	Nickel	6	Nitrogen	NR
Ytterbium		Cadmium		Cobalt	0.6	Carbon	NR
Thulium		Silver		Iron	10	Boron	0.2
Erbium		Palladium		Manganese	0.4	Beryllium	
Holmium		Rhodium		Chromium	0.4	Lithium	0.5
Dysprosium		*Heterogeneous				Hydrogen	NR
		**Probable Contamination From					

STD — Internal Standard

NR — Not Reported

All elements not detected <

MC — Major Component >

INT — Interference

0.7 ppm
100 ppm

Approved:

gh
5-33

Robert L. Taylor
16 May 84

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 1919 SOUTH HIGHLAND AVE., SUITE 210-B, LOMBARD, ILLINOIS 60148 AREA CODE 312 953-9300

Reply to

INSTRUMENTAL ANALYSIS DIVISION, 490 ORCHARD STREET, GOLDEN, COLORADO 80401, PHONE: 303 278-9521



To: Acurex Corporation
555 Clyde Avenue
P.O. Box 7555
Mountain View, CA 94039

Date: May 16, 1984

Analyst: G. Meagher

P. O. No.: Subcontract SW59159A, Release #15, Project #EE7734.82

Sample No.: 901441
EOR Fuel
Test 2

SPARK SOURCE MASS SPECTROGRAPHIC ANALYSIS
CONCENTRATION IN PPM WEIGHT

IAD No.: 97-P137-116-10

ELEMENT	CONC.	ELEMENT	CONC.	ELEMENT	CONC.	ELEMENT	CONC.
Uranium		Terbium		Ruthenium		Vanadium	2
Thorium		Gadolinium		Molybdenum	0.3	Titanium	4
Bismuth		Europium		Niobium	0.03	Scandium	≤0.03
Lead	0.5	Samarium		Zirconium	0.06	Calcium	5
Thallium		Neodymium		Yttrium	0.04	Potassium	3
Mercury	NR	Praseodymium		Strontium	0.2	Chlorine	19
Gold		Cerium		Rubidium		Sulfur	MC
Platinum		Lanthanum		Bromine	0.06	Phosphorus	2
Iridium		Barium	0.3	Selenium	0.4	Silicon	9
Osmium		Cesium		Arsenic	0.05	Aluminum	1
Rhenium		Iodine	0.5	Germanium	≤0.02	Magnesium	5
Tungsten		Tellurium		Gallium	0.2	Sodium	MC
Tantalum		Antimony		Zinc	2	Fluorine	≈4
Hafnium		Tin		Copper	0.7	Oxygen	NR
Lutetium		Indium	STD	Nickel	20	Nitrogen	NR
Ytterbium		Cadmium		Cobalt	0.2	Carbon	NR
Thulium		Silver		Iron	5	Boron	0.08
Erbium		Palladium		Manganese	0.3	Beryllium	<0.01
Holmium		Rhodium		Chromium	0.4	Lithium	0.2
Dysprosium						Hydrogen	NR

STD — Internal Standard

NR — Not Reported

All elements not detected < 0.02 ppm
> 100 ppm

MC — Major Component

INT — Interference

Approved: *Robert L. Taylor*
gh

5-34

16 May 84

COMMERCIAL TESTING & ENGINEERING CO.

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Reply to

INSTRUMENTAL ANALYSIS DIVISION, 490 ORCHARD STREET, GOLDEN, COLORADO 80401, PHONE: 303 278-9521

To: Acurex Corporation
555 Clyde Avenue
P.O. Box 7555
Mountain View, CA 94039



Date: May 16, 1984

Analyst: G. Meagher

P. O. No.: Subcontract SW59159A Release 15 Project 7601

Sample No.: 901458
EOR Filter

SPARK SOURCE MASS SPECTROGRAPHIC ANALYSIS IAD No.: 97-P137-116-10

CONCENTRATION IN PPM WEIGHT of the Filter

ELEMENT	CONC.	ELEMENT	CONC.	ELEMENT	CONC.	ELEMENT	CONC.
Uranium	1	Terbium	0.8	Ruthenium		Vanadium	MC
Thorium	8	Gadolinium	4	Molybdenum	12	Titanium	44
Bismuth	0.2	Europium	0.4	Niobium	0.8	Scandium	4
Lead	3	Samarium	4	Zirconium	3	Calcium	MC
Thallium	0.4	Neodymium	12	Yttrium	24	Potassium	MC
Mercury	NR	Praseodymium	4	Strontium	16	Chlorine	MC
Gold		Cerium	12	Rubidium	0.8	Sulfur	MC
Platinum		Lanthanum	16	Bromine	8	Phosphorus	MC
Iridium		Barium	36	Selenium	4	Silicon	MC
Osmium		Cesium	0.4	Arsenic	16	Aluminum	MC
Rhenium		Iodine	0.8	Germanium	2	Magnesium	MC
Tungsten	0.4	Tellurium	3	Gallium	12	Sodium	MC
Tantalum	2	Antimony	8	Zinc	64	Fluorine	≈170
Hafnium		Tin	4	Copper	8	Oxygen	NR
Lutetium	0.4	Indium	STD	Nickel	MC	Nitrogen	NR
Ytterbium	1	Cadmium	0.2	Cobalt	56	Carbon	NR
Thulium	0.4	Silver	1	Iron	MC	Boron	1
Erbium	2	Palladium		Manganese	20	Beryllium	0.4
Holmium	2	Rhodium		Chromium	36	Lithium	17
Dysprosium	4					Hydrogen	NR

STD — Internal Standard

NR — Not Reported

All elements not detected < 0.1 ppm

MC — Major Component >1000 ppm

INT — Interference

Approved:
5-35

Robert L. Jaylor
16 May 84

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 1919 SOUTH HIGHLAND AVE., SUITE 210-B, LOMBARD, ILLINOIS 60148 AREA CODE 312 953-9300
INSTRUMENTAL ANALYSIS DIVISION, 490 ORCHARD STREET, GOLDEN, COLORADO 80401, PHONE: 303 278-9521

Reply to

To: Acurex Corporation
555 Clyde Avenue
P.O. Box 7555
Mountain View, CA 94039



Date: May 16, 1984

Analyst: G. Meagher

P. O. No.: Subcontract SW59159A Release 15 Project 7601

Sample No.: 901459 SPARK SOURCE MASS SPECTROGRAPHIC ANALYSIS IAD No.: 97-P137-116-10
EOR Filter Blank CONCENTRATION IN PPM WEIGHT of the Filter

ELEMENT	CONC.	ELEMENT	CONC.	ELEMENT	CONC.	ELEMENT	CONC.
Uranium		Terbium		Ruthenium		Vanadium	3
Thorium		Gadolinium		Molybdenum	2	Titanium	24
Bismuth		Europium		Niobium	<0.2	Scandium	0.3
Lead		Samarium		Zirconium	3	Calcium	MC
Thallium		Neodymium		Yttrium	0.8	Potassium	56
Mercury	NR	Praseodymium	0.2	Strontium	4	Chlorine	64
Gold		Cerium	0.1	Rubidium	<0.1	Sulfur	24
Platinum		Lanthanum	0.2	Bromine	2	Phosphorus	12
Iridium		Barium	28	Selenium	0.2	Silicon	84
Osmium		Cesium		Arsenic	0.2	Aluminum	MC
Rhenium		Iodine	0.2	Germanium	0.1	Magnesium	340
Tungsten		Tellurium		Gallium	0.3	Sodium	240
Tantalum		Antimony		Zinc	4	Fluorine	≈64
Hafnium		Tin		Copper	2	Oxygen	NR
Lutetium		Indium	STD	Nickel	12	Nitrogen	NR
Ytterbium		Cadmium	<0.3	Cobalt	<0.3	Carbon	NR
Thulium		Silver		Iron	80	Boron	4
Erbium	8.	Palladium		Manganese	2	Beryllium	
Holmium		Rhodium		Chromium	8	Lithium	0.8
Dysprosium						Hydrogen	NR

STD — Internal Standard

NR — Not Reported

All elements not detected <0.2 ppm

MC — Major Component >1000 ppm

INT — Interference

Approved: 5-36

Robert L. Taylor
16 May 84

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 1919 SOUTH HIGHLAND AVE., SUITE 210-B, LOMBARD, ILLINOIS 60148 AREA CODE 312 953-9300
INSTRUMENTAL ANALYSIS DIVISION, 490 ORCHARD STREET, GOLDEN, COLORADO 80401, PHONE: 303 278-9521

Reply to



To: Acurex Corporation
555 Clyde Avenue
P.O. Box 7555
Mountain View, CA 94039

Date: May 16, 1984

Analyst: G. Meagher

P. O. No.: Subcontract SW59159A, Release # 15, Project #EE7734.82

Sample No.: 901454
EOR XAD-2

SPARK SOURCE MASS SPECTROGRAPHIC ANALYSIS

IAD No.: 97-P137-116-10

CONCENTRATION IN PPM WEIGHT

ELEMENT	CONC.	ELEMENT	CONC.	ELEMENT	CONC.	ELEMENT	CONC.
Uranium		Terbium		Ruthenium		Vanadium	0.09
Thorium		Gadolinium		Molybdenum	0.8	Titanium	4
Bismuth		Europium		Niobium		Scandium	0.2
Lead	0.4	Samarium		Zirconium	0.1	Calcium	17
Thallium		Neodymium		Yttrium		Potassium	12
Mercury	NR	Praseodymium		Strontium	0.2	Chlorine	4
Gold		Cerium		Rubidium		Sulfur	6
Platinum	*0.6	Lanthanum		Bromine		Phosphorus	2
Iridium		Barium	0.9	Selenium		Silicon	13
Osmium		Cesium		Arsenic	0.07	Aluminum	1
Rhenium		Iodine	0.1	Germanium	0.05	Magnesium	9
Tungsten		Tellurium		Gallium	0.08	Sodium	3
Tantalum		Antimony		Zinc	3	Fluorine	≈8
Hafnium		Tin		Copper	0.4	Oxygen	NR
Lutetium		Indium	STD	Nickel	0.6	Nitrogen	NR
Ytterbium		Cadmium		Cobalt	0.04	Carbon	NR
Thulium		Silver		Iron	5	Boron	0.7
Erbium		Palladium		Manganese	0.4	Beryllium	
Holmium		Rhodium		Chromium	0.4	Lithium	0.3
Dysprosium		*Probable Contamination From Sample Preparation				Hydrogen	NR

STD — Internal Standard

NR — Not Reported

All elements not detected < 0.08 ppm

MC — Major Component > 100 ppm

INT — Interference

Approved:
5-37

Robert L. Taylor
16 May 84

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 1919 SOUTH HIGHLAND AVE., SUITE 210-B, LOMBARD, ILLINOIS 60148 AREA CODE 312 953-9300

INSTRUMENTAL ANALYSIS DIVISION, 490 ORCHARD STREET, GOLDEN, COLORADO 80401, PHONE: 303 278-9521

Reply to

To: Acurex Corporation
555 Clyde Avenue
P.O. Box 7555
Mountain View, CA 94039



Date: May 16, 1984

Analyst: G. Meagher

P. O. No.: Subcontract SW59159A, Release # 15, Project #EE7734.82

Sample No.: 901475 SPARK SOURCE MASS SPECTROGRAPHIC ANALYSIS
EOR XAD-2 Blank CONCENTRATION IN PPM WEIGHT

IAD No.: 97-P137-116-10

ELEMENT	CONC.	ELEMENT	CONC.	ELEMENT	CONC.	ELEMENT	CONC.
Uranium		Terbium		Ruthenium		Vanadium	0.07
Thorium		Gadolinium		Molybdenum	0.7	Titanium	5
Bismuth		Europium		Niobium		Scandium	0.3
Lead		Samarium		Zirconium	0.1	Calcium	*13
Thallium		Neodymium		Yttrium		Potassium	4
Mercury	NR	Praseodymium		Strontium	0.09	Chlorine	17
Gold		Cerium		Rubidium		Sulfur	1
Platinum	**0.3	Lanthanum		Bromine		Phosphorus	3
Iridium		Barium	0.5	Selenium		Silicon	15
Osmium		Cesium		Arsenic	0.04	Aluminum	1
Rhenium		Iodine	0.09	Germanium	≤0.04	Magnesium	8
Tungsten		Tellurium		Gallium	0.08	Sodium	8
Tantalum		Antimony		Zinc	0.7	Fluorine	~44
Hafnium		Tin		Copper	0.6	Oxygen	NR
Lutetium		Indium	STD	Nickel	0.5	Nitrogen	NR
Ytterbium		Cadmium	0.1	Cobalt	≤0.07	Carbon	NR
Thulium		Silver		Iron	6	Boron	0.2
Erbium		Palladium		Manganese	0.3	Beryllium	
Holmium		Rhodium		Chromium	0.5	Lithium	0.3
Dysprosium		*Heterogeneous				Hydrogen	NR
		**Probable Contamination From					
		Sample Preparation					

STD — Internal Standard

NR — Not Reported

All elements not detected < 0.04 ppm
MC — Major Component > 100 ppm

INT — Interference

Approved: *Robert L. Daylen*

5-38

16 May 84

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 1919 SOUTH HIGHLAND AVE., SUITE 210-B, LOMBARD, ILLINOIS 60148 AREA CODE 312 953-9300
INSTRUMENTAL ANALYSIS DIVISION, 490 ORCHARD STREET, GOLDEN, COLORADO 80401, PHONE: 303 278-9521

Reply to



To: Acurex Corporation
555 Clyde Avenue
P.O. Box 7555
Mountain View, CA 94039

Date: May 16, 1984

Analyst: G. Meagher

P. O. No.: Subcontract SW59159A, Release # 15, Project #EE7734.82

Sample No.: XAD-2 SPARK SOURCE MASS SPECTROGRAPHIC ANALYSIS
Preparation Reagent Blank

IAD No.: 97-P137-116-10

CONCENTRATION IN PPM WEIGHT

ELEMENT	CONC.	ELEMENT	CONC.	ELEMENT	CONC.	ELEMENT	CONC.
Uranium	≤0.4	Terbium		Ruthenium		Vanadium	0.04
Thorium	0.8	Gadolinium		Molybdenum	≤0.2	Titanium	0.6
Bismuth		Europium		Niobium		Scandium	0.2
Lead	1	Samarium		Zirconium	0.4	Calcium	11
Thallium		Neodymium	0.6	Yttrium	0.2	Potassium	7
Mercury	NR	Praseodymium	0.4	Strontium	0.2	Chlorine	8
Gold	**2	Cerium	1	Rubidium		Sulfur	1
Platinum		Lanthanum	1-	Bromine		Phosphorus	10
Iridium		Barium	0.6	Selenium		Silicon	*20
Osmium		Cesium		Arsenic	0.1	Aluminum	2
Rhenium		Iodine	0.06	Germanium	0.02	Magnesium	52
Tungsten		Tellurium		Gallium	0.2	Sodium	5
Tantalum		Antimony		Zinc	4	Fluorine	≈40
Hafnium		Tin		Copper	1	Oxygen	NR
Lutetium		Indium	STD	Nickel	0.6	Nitrogen	NR
Ytterbium		Cadmium		Cobalt	0.06	Carbon	NR
Thulium		Silver	0.2	Iron	18	Boron	0.2
Erbium		Palladium		Manganese	0.2	Beryllium	
Holmium		Rhodium		Chromium	0.2	Lithium	0.6
Dysprosium		*Heterogeneous				Hydrogen	
		**Probable Contamination					

STD — Internal Standard

NR — Not Reported

All elements not detected < 0.04 ppm
MC — Major Component > 100 ppm

INT — Interference

Approved: gh

5-39

Robert L. Taylor
16 May 84

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 1919 SOUTH HIGHLAND AVE., SUITE 210-B, LOMBARD, ILLINOIS 60148 AREA CODE 312 953-9300
INSTRUMENTAL ANALYSIS DIVISION, 490 ORCHARD STREET, GOLDEN, COLORADO 80401, PHONE: 303 278-9521

Reply to

To: Acurex Corporation
555 Clyde Avenue
P.O. Box 7555
Mountain View, CA 94039



Date: May 16, 1984

Analyst: G. Meagher

P. O. No.: Subcontract SW59159A, Release #15, Project #EE7734.82

Sample No.: 901463

SPARK SOURCE MASS SPECTROGRAPHIC ANALYSIS

IAD No.: 97-P137-116-10

EOR

Impinger 1

CONCENTRATION IN $\mu\text{g/mL}$

ELEMENT	CONC.	ELEMENT	CONC.	ELEMENT	CONC.	ELEMENT	CONC.
Uranium		Terbium		Ruthenium		Vanadium	0.05
Thorium		Gadolinium		Molybdenum	1	Titanium	1
Bismuth		Europium		Niobium	≤ 0.04	Scandium	0.5
Lead	6	Samarium		Zirconium	0.06	Calcium	2
Thallium		Neodymium		Yttrium	0.01	Potassium	2
Mercury	NR	Praseodymium	0.01	Strontium	0.1	Chlorine	5
Gold		Cerium		Rubidium	0.01	Sulfur	MC
Platinum		Lanthanum		Bromine	0.2	Phosphorus	2
Iridium		Barium	0.2	Selenium	0.5	Silicon	4
Osmium		Cesium	0.004	Arsenic	0.05	Aluminum	0.9
Rhenium		Iodine	0.1	Germanium	0.09	Magnesium	MC
Tungsten		Tellurium	0.09	Gallium	0.04	Sodium	MC
Tantalum		Antimony	0.03	Zinc	MC	Fluorine	MC
Hafnium		Tin	0.2	Copper	MC	Oxygen	NR
Lutetium		Indium	STD	Nickel	3	Nitrogen	NR
Ytterbium		Cadmium	≤ 0.02	Cobalt	≤ 0.01	Carbon	NR
Thulium		Silver	0.09	Iron	6	Boron	0.02
Erbium		Palladium		Manganese	0.2	Beryllium	
Holmium	≤ 0.2	Rhodium		Chromium	3	Lithium	0.08
Dysprosium						Hydrogen	NR

STD — Internal Standard

NR — Not Reported

All elements not detected $< 0.008 \mu\text{g/mL}$

MC — Major Component $> 10 \mu\text{g/mL}$

INT — Interference

Approved:

gh
5-40

Robert L. Jay
16 May 84

COMMERCIAL TESTING & ENGINEERING CO.

GENERAL OFFICES: 1919 SOUTH HIGHLAND AVE., SUITE 210-B, LOMBARD, ILLINOIS 60148 AREA CODE 312 953-9300

INSTRUMENTAL ANALYSIS DIVISION, 490 ORCHARD STREET, GOLDEN, COLORADO 80401, PHONE: 303 278-9521

Reply to

To: Acurex Corporation
555 Clyde Avenue
P.O. Box 7555
Mountain View, CA 94039



Date: May 16, 1984

Analyst: G. Meagher

P. O. No.: Subcontract SW59159A, Release #15, Project #EE7734.82

Sample No.: 901461
EOR Impinger
1 Blank

SPARK SOURCE MASS SPECTROGRAPHIC ANALYSIS

IAD No.: 97-P137-116-10

CONCENTRATION IN $\mu\text{g/mL}$

ELEMENT	CONC.	ELEMENT	CONC.	ELEMENT	CONC.	ELEMENT	CONC.
Uranium		Terbium		Ruthenium		Vanadium	0.003
Thorium		Gadolinium		Molybdenum	0.03	Titanium	0.04
Bismuth		Europium		Niobium	≤ 0.004	Scandium	0.005
Lead		Samarium		Zirconium	0.01	Calcium	0.4
Thallium		Neodymium		Yttrium		Potassium	0.2
Mercury	NR	Praseodymium		Strontium	0.003	Chlorine	*6
Gold		Cerium		Rubidium		Sulfur	MC
Platinum		Lanthanum		Bromine	0.008	Phosphorus	1
Iridium		Barium	0.02	Selenium	0.006	Silicon	0.6
Osmium		Cesium		Arsenic	≤ 0.002	Aluminum	0.05
Rhenium		Iodine	0.03	Germanium	≤ 0.002	Magnesium	0.7
Tungsten		Tellurium	0.006	Gallium	0.003	Sodium	MC
Tantalum		Antimony	≤ 0.009	Zinc	0.02	Fluorine	≈ 0.3
Hafnium		Tin	0.2	Copper	0.002	Oxygen	NR
Lutetium		Indium	STD	Nickel	0.01	Nitrogen	NR
Ytterbium		Cadmium		Cobalt	0.004	Carbon	NR
Thulium		Silver		Iron	0.06	Boron	0.002
Erbium		Palladium		Manganese	0.01	Beryllium	
Holmium		Rhodium		Chromium	0.01	Lithium	0.01
Dysprosium		*Heterogeneous				Hydrogen	NR

STD — Internal Standard

NR — Not Reported

All elements not detected $< 0.003 \mu\text{g/mL}$

MC — Major Component $> 10 \mu\text{g/mL}$

INT — Interference

Approved: *Robert L. Jorgensen*

5-41

16 May 84

COMMERCIAL TESTING & ENGINEERING CO.

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GERALD T. SKAR
MANAGER
INSTRUMENTAL ANALYSIS DIVISION



PLEASE ADDRESS ALL CORRESPONDENCE TO:
490 ORCHARD ST., GOLDEN, CO. 80401
OFFICE TEL. (303) 278-9521

August 2, 1984

Mr. Larry Waterland
Acurex Corporation
P.O. Box 7555
Mountain View, CA 94039

RE: IAD #97-P897-116-06
Subcontract #SW 59159A
Release #16

Analytical Report

Six samples, previously analyzed for trace elements by spark source mass spectrometry, under our IAD identification #97-P137-116-10, were logged in under our IAD identification #97-P897-116-06 on July 16, 1984, for additional analysis.

Chlorine and fluorine were determined using specific ion electrode methodology. Phosphorus was determined colorimetrically.

Depending on sample type and the amount of sample available, sulfur was determined turbidimetrically or by X-ray fluorescence spectrometry.

The remaining elemental analysis was performed using flame atomic absorption/emission spectrophotometry.

The results of these determinations are presented in the following tables. Samples #1 and 2 are reported in total micrograms (μg) on the filter. Samples #3 and 4 are reported in micrograms per millilitre ($\mu\text{g/mL}$). Samples #5 and 6 are reported in micrograms per gram ($\mu\text{g/g}$). All values are reported on an "as received" basis.

If you have any questions concerning these results, please call.


Harold A. Connell
Project Coordinator

HAC/as



Charter Member

Table No. I
(Total μg on the Filter)

<u>Parameter</u>	<u>#1 - 901458</u> <u>EOR Filter</u>	<u>#2 - 901459</u> <u>EOR Filter Blank</u>
Aluminum, (Al)	7,000	3,740
Calcium, (Ca)	16,000	--
Chlorine, (Cl)	44,300	--
Iron, (Fe)	10,150	--
Potassium, (K)	80	--
Magnesium, (Mg)	2,640	--
Sodium, (Na)	1,930	--
Nickel, (Ni)	33,100	--
Phosphorus, (P)	590	--
Sulfur, (S)	125	--
Silicon, (Si)	780	--
Vanadium, (V)	1,320	--

Table No. II
($\mu\text{g}/\text{mL}$)

<u>Parameter</u>	<u>#3 - 901463</u> <u>EOR Impinger 1</u>	<u>#4 - 901461</u> <u>EOR Impinger 1 Blank</u>
Copper, (Cu)	71.9	--
Fluorine, (F)	0.89	--
Magnesium, (Mg)	0.14	--
Sodium, (Na)	4,960	0.39
Sulfur, (S)	6,920	<50
Zinc, (Zn)	30	--

Table No. III
($\mu\text{g}/\text{g}$)

<u>Parameter</u>	<u>#5 - 901440</u> <u>EOR Fuel, Test 1</u>	<u>#6 - 901441</u> <u>EOR Fuel, Test 2</u>
Chlorine, (Cl)	25	21
Sodium, (Na)	132	104
Sulfur, (S)	11,700	11,600

5.7 ORGANIC ANALYSES OF SASS SAMPLES: TOTAL CHROMATOGRAPHABLE ORGANICS (TCO), GRAVIMETRIC ORGANICS (GRAV), GAS CHROMATOGRAPHY MASS SPECTROMETRY (GC/MS), and INFRARED (IR) SPECTRA OF TOTAL SAMPLE EXTRACTS

Acurex/ES
MS 2-2260April 18, 1984
Acurex ID#: 8402-006
Client PO#: 307736.82

Attention: Larry Waterland

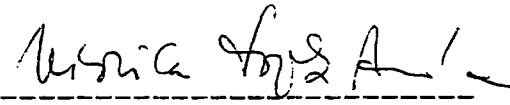
Sample: Bakersfield, 1 SASS Train;
Received 2/3/84

The above samples were analyzed by Level 1 protocol. The XAD and OMC extracts were combined per your instruction. Organic extracts were also analyzed for the semivolatile priority pollutants by gas chromatography/mass spectrometry employing a J&W SE-54 30 meter capillary column. The column was held at 30°C for 2 minutes, then ramped at 10°C per minute to 270°C. In addition to the priority pollutants, benzo(c)phenanthrene, dibenzo(c,g)carbazole, 7,12-dimethylbenzo(a)anthracene, 3-methylcholanthrene, and perylene were sought employing the computerized library search and manual interpretation. The assignment and quantitation of these organics is tentative since analytical standards of these compounds were not available for analysis. Benzo(c)phenanthrene, dibenzo(c,g)carbazole, 7-12-dimethylbenzo(a)anthracene, 3-methylcholanthrene and perylene were not detected in any of the samples at levels above 100 ug per train.

After extraction of the XAD field blank, the same resin was spiked with 400 ug each of dodecane and hexadecane for TCO analysis, 400 ug each of naphthalene, phenanthrene, and pyrene for PAH analysis, and 10 mg of bis(2-ethylhexyl)phthalate which combined with the phenanthrene and pyrene for the GRAV analysis. Results are presented in Tables 1 through 3. Chromatograms and spectra are attached.

Submitted by:



Greg Nicoll
Manager, Inorganic Chemistry

Viorica Lopez-Avila, Ph.D.
Technical Director

GN/VLA/ats

Attachments

Table 1. TCO and GRAV Results

<u>Sample ID</u>	<u>TCO</u>	<u>GRAV</u>
Filters	--	<3 mg/train
XAD*	4.1 mg/train	6 mg/train
XAD blank	0.34 mg/train	3 mg/train
XAD spike	784 ug	11 mg
XAD spike level	800 ug**	10.8 mg***
XAD spike recovery	98%	102%

* Blank corrected

** 400 ug each of C(12) and C(16)-alkanes

*** 10 mg of bis(2-ethylhexyl)phthalate, 400 ug of phenanthrene,
and 400 ug of pyrene

Table 2. GC/MS Results, ug/train

Analyte	XAD	XAD*	Spiked XAD	% Recovery of spiked XAD
Dibutylphthalate	<50	<50	NS***	--
Dimethylphthalate	100	60	NS	--
Naphthalene	40	20	420	105
Phenanthrene	<10	<10	400	100
Phenol	20	10	NS	--
Pyrene	<10	<10	510	128
Other Priority Pollutants	ND**	ND	NS	--

* Duplicate injection

** ND - Not detected

*** NS - Not spiked

Table 3. Sample Disposition

Sample ID	Type	Initial	Subcontract	Organic	Remainder
901455 #31	Filter	--	32%	68%	62%*
901456 #32	Filter	--	33%	67%	
901457 #33	Filter	--	28%	72%	
901458 #34	Filter	--	30%	70%	
901459 #35	Filter blank	--	100%	0	0
901453	OMR	395 ml	--	--	--
901454	XAD	130 g	5 g	125 g	87%*
901475	XAD blank	130 g	5 g	125 g	87%*
-----	XAD spike	125 g	0	125 g	90%*
901442 } 901443 } 901444 }	OMC	1910 ml	--	--	--
901463	Imp 1	595 mL**	100 mL	0	2550 mL
901461	Imp 1 blank	1 L	100 mL	0	1 L
901464	Imp 2&3	920 mL	100 mL	0	820 mL
901462	Imp 2&3 blank	1 L	100 mL	0	1 L
901440	Grab fuel 1A	500 mL	100; 100; 100 mL	0	200 mL

* as extract

** Imp 1 & OMC (aqueous) volume is 2650 mL

IR REPORT

SAMPLE:

8402-006-1 Filters

[illegible]

SAMPLE:

8402-006-7 XAD

5-50

IR REPORT

SAMPLE: 8402-006-8 XAD Blank

[illegible]

SAMPLE:

XAD Spike

[illegible]

5.8 VOLATILE ORGANICS ANALYSES OF VOST TRAPS

Inhouse experiments regarding the level of precautions needed to prevent blank trap contamination during storage and shipping were being performed during the time period of these tests. As a consequence, six pairs of trap blanks were available for use in this test: two pairs of trip blanks, two pairs of field blanks, and two pairs of laboratory blanks, differing only in the manner in which they were stored. As suggested by the VOST protocol, the pair t-test was used to assess the "sameness" of each blank trap pair. Use of this test showed all six blank pairs to be the same, with a confidence level of 70 percent or greater. Therefore, a mean blank trap level for each of the volatile compounds determined, with an associated standard deviation, was used to blank-correct each sample trap analyzed. The concentration of a compound had to be present in a sample trap at a level greater than three standard deviations above the mean blank level to be considered actually present in the flue gas sampled (as suggested by the VOST protocol). Based on this criterion, only benzene, toluene, and ethylbenzene were found to be present in sample traps at levels statistically different from blank traps. Thus, only emissions of these three components are reported in Volume 1 of this report.

The analytical data report follows. Traps denoted by the suffix "A" are the Tenax/charcoal trap of a run pair.

Acurex/ES (CMEA)

Attention: Larry Waterland/2-2260

March 9, 1984

Acurex ID#: 8402-004

Client PO#: 307736.82
302865.65

Page 1 of 5

Subject: Analysis of 10 Pairs of Tenax Traps,
Received 2/2/84

The above referenced samples were individually analyzed by GC/MS according to EPA VOST Protocol for volatile organics (EPA Method 624 Priority Pollutants).

Sample Analysis results are listed in Table 1. Blank data and recovery data from spiked Tenax traps are given in Tables 2 and 3, respectively.

If you have any questions, please call.

Prepared by:

William G. Hellier
William G. Hellier
Staff Chemist

Approved by:

Viorica Lopez-Avila
Viorica Lopez-Avila, Ph.D.
Technical Director

WGH/VLA/ats

Table 1. Results of Volatile Organic Analyses

Sample ID Trap #	Concentration (ng/trap)									
	Run #4 7 ^a	Run #4 33A ^a	Field Blank 40 ^a	Field Blank 7A ^a	Trip Blank 42 ^a	Trip Blank 15A ^a	Run #2 23	Run #2 24A ^b	Lab Blank 8	Lab Blank 10A
Priority Pollutants										
Chloromethane	302	4900	2260	27	523	58	960	87	290	53
Dichloromethane	137	2670	550	3050	396	4160	103	933	115	225
1,1-Dichloroethylene	ND	ND	ND	ND	ND	8	ND	6	ND	ND
Trans-1,2-Dichloroethylene	2	ND	ND	ND	ND	ND	ND	ND	ND	3
Chloroform	28	ND	ND	ND	ND	12	24	ND	35	ND
1,2-Dichloroethane	3	ND	ND	ND	ND	24	ND	ND	ND	ND
1,1,1-Trichloroethane	9	19	10	7	9	ND	8	ND	7	3
Carbon tetrachloride	77	ND	ND	ND	12	8	ND	5	ND	5
1,2-Dichloropropane	4	ND	ND	ND	ND	22	4	ND	ND	ND
Trichloroethylene	8	3	ND	12	11	ND	ND	ND	ND	ND
1,1,2-Trichloroethane	29	ND	ND	ND	30	29	ND	ND	ND	ND
Benzene	63	35	10	38	38	51	850	34	14	ND
Tetrachloroethylene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,1,2,2-Tetrachloroethane	47	ND	ND	ND	ND	10	ND	6	ND	11
Toluene	67	42	7	35	29	16	33	52	13	52
Chlorobenzene	10	ND	ND	ND	ND	12	ND	4	ND	ND
Ethylbenzene	8	6	2	29	ND	ND	1	ND	1	ND
Nonpriority Pollutants										
Xylenes	11	9	4	30	8	15	7	10	5	15
Detection Limit	2	2	2	2	2	2	1	1	1	1
Percent Surrogate Recovery										
Toluene-d ₈	65	86	13 ^c	146	219	100	79	136	80	107

a - Shipped in wooden boxes

b - Transport tube received broken

c - Low recovery of internal standards

ND - Not detected

Table 1. Results of Volatile Organic Analyses (Cont.)

Sample ID Trap #	Concentration (ng/trap)									
	Glass Sealed 44	Glass Sealed 20A	Run #1 45	Run #1 19A	Run #3 21 ^{a,b}	Run #3 13 ^b	Field Blank 11	Field Blank 32A	Trip Blank 9	Trip Blank 35A
Priority Pollutants										
Chloromethane	830	37	519	146	2240	66	721	28	1340	71
Vinyl Chloride	ND	ND	ND	9	ND	ND	ND	ND	ND	ND
Dichloromethane	120	121	109	25200	63	889	115	1550	118	204
1,1-Dichloroethylene	ND	10	ND	3	ND	ND	ND	ND	22	ND
Trans-1,2-Dichloroethylene	ND	ND	ND	3	ND	ND	ND	ND	ND	ND
Chloroform	ND	ND	24	ND	ND	ND	3	ND	ND	3
1,2-Dichloroethane	ND	12	8	ND	ND	ND	ND	ND	ND	ND
1,1,1-Trichloroethane	ND	15	30	ND	8	10	ND	3	20	10
Carbon Tetrachloride	ND	8	ND	ND	46	ND	ND	ND	ND	ND
1,2-Dichloropropane	ND	ND	27	17	ND	ND	ND	ND	ND	ND
Trichloroethylene	ND	ND	8	6	ND	ND	5	ND	ND	ND
1,1,2-Trichloroethane	ND	ND	ND	54	ND	ND	ND	ND	ND	ND
Benzene	19	5	2640	ND	205	46	26	1	20	41
Tetrachloroethylene	ND	17	11	32	ND	21	ND	4	ND	ND
1,1,2,2-Tetrachloroethane	ND	8	ND	ND	ND	ND	ND	3	ND	8
Toluene	10	42	144	2	57	34	2	2	9	44
Ethylbenzene	3	9	9	72	4	5	ND	2	4	7
Nonpriority Pollutants										
Styrene	1	ND	2	6	ND	ND	ND	ND	3	6
Xylenes	2	ND	8	ND	6	10	4	7	3	9
Detection Limit	1	1	2	2	2	2	2	2	2	2
Percent Surrogate Recovery										
Toluene-d ₈	108	134	91	213 ^c	95	142	111	103	106	142

a - Transport tube received broken
 b - Transported with activated charcoal
 c - Low recovery of internal standards
 ND - Not Detected

Table 2. Analysis Blanks

Sample ID Date	Concentration (ng/Trap)							
	Purge Blank 2/2/84	Trap Blank 2/2/84	Purge Blank 2/3/84	Trap Blank 2/3/84	Purge Blank 2/5/84	Trap Blank 2/5/84	Purge Blank 2/6/84	Trap Blank 2/6/84
<u>Priority Pollutants</u>								
Chloromethane	70	286	4	315	17	2130	63	64
Dichloromethane	78	60	81	68	49	62	115	59
1,1-Dichloroethylene	ND	14	ND	ND	ND	ND	ND	ND
1,2-Dichloroethane	ND	7	ND	ND	ND	ND	ND	11
1,1,1-Trichloroethane	ND	59	ND	ND	ND	ND	ND	ND
Trichloroethylene	4	23	ND	2	ND	ND	ND	ND
Chlorodibromomethane	ND	ND	ND	ND	ND	15	ND	ND
1,1,2-Trichloroethane	ND	10	ND	6	ND	24	ND	ND
Benzene	18	41	14	18	12	26	2	19
Tetrachloroethylene	2	3	ND	21	ND	ND	ND	ND
1,1,2,2-Tetrachloroethane	6	13	ND	23	ND	41	ND	ND
Toluene	4	12	3	10	5	12	ND	12
Chlorobenzene	ND	ND	ND	7	ND	ND	ND	ND
Ethylbenzene	3	3	3	8	1	9	NO	7
<u>Nonpriority Pollutants</u>								
Styrene	3	2	ND	7	ND	3	5	10
Xylenes	4	5	5	9	ND	ND	52	10
Detection Limit	2	2	2	2	2	2	2	2
<u>Percent Surrogate Recovery</u>								
Toluene-d ₈	100	95	93	91	96	102	104	109

ND - Not detected

Table 3. Tenax Trap Spike Recovery

Sample ID Date	% Recovery			
	200 ng Trap 2/2/84	200 ng Trap 2/3/84	200 ng Trap 2/5/84	200 ng Trap 2/6/84
Chloromethane	404	615	338	49
Bromomethane	116	160	114	90
Vinyl chloride	112	163	117	74
Chloroethane	116	170	100	70
Dichloromethane	116	136	109	106
1,1-Dichloroethylene	131	171	112	73
1,1-Dichloroethane	128	161	114	84
Trans-1,2-Dichloroethylene	130	170	114	78
Chloroform	130	154	110	88
1,2-Dichloroethane	94	87	82	70
1,1,1-Trichloroethane	118	158	108	78
Carbon tetrachloride	118	161	110	60
Dichlorobromomethane	100	95	91	68
1,2-Dichloropropane	93	65	96	139
Trichloroethylene	90	66	101	111
1,1,2-Trichloroethane	39	54	113	58
Benzene	118	96	138	152
Tetrachloroethylene	100	78	102	84
Toluene	106	67	110	91
Chlorobenzene	66	31	68	43
Ethylbenzene	85	38	81	44
<u>Nonpriority Pollutants</u>				
Xylenes	66	42	54	54
<u>Percent Surrogate Recovery</u>				
Toluene-d ₈	104	72	105	95

5.9 N₂O EMISSIONS BY GC/ECD

Acurex/ES

May 21, 1984

Acurex ID#: 8404-025

Client PO#: 307736.82

Page 1 of 1

Attention: Larry Waterland

Subject: Analysis of 3 Gas Bombs for Nitrous Oxide by GC/ECD

The above referenced samples were analyzed by GC/ECD according to previously reported method.

Results are listed in the table below:

<u>Sample ID</u>	<u>N₂O (ppm)</u>
901428	<0.5*
901448	2
901470	11

* Sample cylinder was not pressurized -
sample may have leaked.

If you have any questions, please call.

Prepared by:

William G. Hellier
Staff Chemist

Approved by:

Richard B. Scott for
Viorica Lopez-Avila, Ph.D.
Technical Director

WGH/VLA/ats

5.10 NO_x EMISSIONS BY EPA METHOD 7

Laboratory analysis data for the Method 7 test performed on January 24, 1984, was included on the forms reporting the sampling and recovery data included in Section 4.2. Analysis data for the tests performed on February 8 and 24, 1984, appear on the following pages.

ACUREX ANALYTICAL REPORT

Sample of: CMEA/EER Bakara field

Sample Date: 2-8-84

Requested By: Larry Waterland

I.D. Number: 307735-82

Analytical Method: EPA METHOD 7 NOX ANALYSIS

Date of Analysis: 3-29-84 : Test date = 2-8-84

Lab I.D. Number	TEST #	Analytical Result		Unit
900573	1	185.6	92.8	mg NO ₂ / mg/dscm i.d.
900572	2	123.8	61.9	
900559	3	88.4	44.2	
900563	4	293.2	146.6	
900548	5	366.6	183.3	
900568	6	235.4	117.7	
900564	7	244.4	122.2	
900561	8	283.0	141.5	
900562	9	229.0	114.5	
900560	10	267.6	133.8	
900570	11	360.2	180.1	
900575	12	373.0	186.5	
900571	13	326.8	163.4	

Analysis By: K. Brent

5-62

Date: 3-29-84

ACUREX ANALYTICAL REPORT

Sample of: CMEA/EER Bakerafield

Sample Date: 2-8-84

Requested By: Larry Waterland

I.D. Number: 307735.82

Analytical Method: EPA METHOD 7 NOx ANALYSIS

Date of Analysis: 3-27-84 :

Lab I.D. Number	TEST #	Analytical Result		Unit
900555	14	57.8	28.9	mg/dscm NO ₂
900547	15	292.0	146.0	
900537	16	283.0	141.5	
900574	17	48.8	24.4	
900565	18	328.0	164.0	
900566	19	345.2	157.6	
900549	20	224.6	112.3	
900567	21	191.6	95.8	
900534	22	218.6	109.3	
900558	23	220.0	110.0	
900569	24	196.8	98.4	
900551	25	159.6	79.8	
900550	26	236.8	118.3	
EPA QA sample #0481		594.68	297.34*	

*Actual value = 298.5 mg/dscm NO₂

5-63

Analysis By: C. J. Brunton

Date: 3-29-84

ACUREX ANALYTICAL REPORT

Sample of: CMEA/EER Bakara field

Sample Date: 2-24-84

Requested By: Larry Waterland

I.D. Number: 307735.82

Analytical Method: EPA METHOD 7 NOX ANALYSIS

Date of Analysis: 3-28-84

Lab I.D. Number	TEST #	Analytical Result		Unit
903474	1	262.7	131.35	mg/m ³ / mg/dscm/NL
903475	2	223.8	111.9	
903476	3	189.99	94.99	
903477	4	257.62	128.81	
903478	5	295.45	147.72	
903479	6	378.37	189.18	
903480	7	265.66	132.83	
903481	8	118.38	59.19	
903482	9	251.18	125.59	
903483	10	547.43	273.72	

Analysis By: [Signature]

5-64

Date: 3-29-84

TECHNICAL REPORT DATA <i>(Please read Instructions on the reverse before completing)</i>		
1. REPORT NO. EPA-600/7-86-013b	2.	3. RECIPIENT'S ACCESSION NO.
4. TITLE AND SUBTITLE Environmental Assessment of an Enhanced Oil Recovery Steam Generator Equipped with an EPA Heavy-oil Low-NOx Burner; Volume II*	5. REPORT DATE April 1986	
	6. PERFORMING ORGANIZATION CODE	
7. AUTHOR(S) C. Castaldini, L.R. Waterland, and R. De Rosier	8. PERFORMING ORGANIZATION REPORT NO.	
9. PERFORMING ORGANIZATION NAME AND ADDRESS Acurex Corporation Energy and Environmental Division P.O. Box 7044 Mountain View, California 94039	10. PROGRAM ELEMENT NO.	
	11. CONTRACT/GRANT NO. 68-02-3188	
12. SPONSORING AGENCY NAME AND ADDRESS EPA, Office of Research and Development Air and Energy Engineering Research Laboratory Research Triangle Park, NC 27711	13. TYPE OF REPORT AND PERIOD COVERED Final; 1/84 - 1/85	
	14. SPONSORING AGENCY CODE EPA/600/13	
15. SUPPLEMENTARY NOTES AEERL project officer is Joseph A. McSorley, Mail Drop 65, 919/541-2920. Volume I contains technical results. (*) Volume II is Data Supplement.		
16. ABSTRACT The report gives results of comprehensive emission measurements and 30-day flue gas monitoring on a 16-MW (55 million Btu/hr) enhanced oil recovery steam generator equipped with the EPA low-NOx burner firing high-nitrogen crude. The 1-day comprehensive measurements included quantification of semivolatile organics and 73 trace elements; volatile organic sampling train quantitation of volatile organic priority pollutants; EPA Method 5/8 for particulate and SOx; controlled condensation for SOx; Andersen impactors for particle size distribution; grab samples for N2O; and continuous flue gas monitoring. NOx emissions averaged 70 ppm at 3% O2, well below the target of 85 ppm. CO emissions were below 30 ppm, and SO2 averaged about 550 ppm. Solid particulates were emitted at about 27 ng/J (96 mg/dscm); condensible particulates were about half that. Volatile organics (benzene, toluene, and ethylbenzene) were measured in the 0.4 to 20 ppb range. Semivolatile organics (naphthalene and phenol) were detected at about 0.3 ppb. Subsequent continuous monitoring of flue gas criteria emissions showed NOx below 80 ppm at 3% O2 with an average of 70 ppm. CO emissions were generally less than 30 ppm.		
17. KEY WORDS AND DOCUMENT ANALYSIS		
a. DESCRIPTORS	b. IDENTIFIERS/OPEN ENDED TERMS	c. COSATI Field/Group
Pollution Assessments Boilers Oil Recovery Crude Oil Combustion	Pollution Control Stationary Sources Environmental Assessment Low-NOx Burners	13B 14B 13A 08I, 11H 21B
18. DISTRIBUTION STATEMENT Release to Public	19. SECURITY CLASS (This Report) Unclassified	21. NO. OF PAGES 187
	20. SECURITY CLASS (This page) Unclassified	22. PRICE