

PROCEEDINGS OF THE EPA/INDUSTRY  
QUALITY CONTROL SYMPOSIUM

INTRA-LABORATORY TEST SITE/EQUIPMENT  
QUALITY CONTROL TECHNIQUES

October 5, 1977

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QUALITY CONTROL SYMPOSIUM

INTRA-LABORATORY TEST SITE/EQUIPMENT  
QUALITY CONTROL TECHNIQUES

October 5, 1977  
9:00 A.M. - 4:00 P.M.

HELD AT:  
Environmental Protection Agency  
2565 Plymouth Road  
Ann Arbor, Michigan 48103

Symposium Chairman:  
Frank E. Johnson  
Emission Development Testing  
Chrysler Corporation  
Detroit, Michigan 48288

SUMMARY REPORT  
EPA/INDUSTRY QUALITY CONTROL SYMPOSIUM  
INTRA-LABORATORY TEST SITE/EQUIPMENT  
QUALITY CONTROL TECHNIQUES

INTRODUCTION:

This report summarizes the proceedings, information, discussions and presentations made at the Fourth Quality Control Symposium held at the Environmental Protection Agency Laboratory, Ann Arbor, Michigan, on October 5, 1977.

As in the previous meetings, this symposium was a joint EPA/Automotive Industry effort to discuss the Quality Control techniques used to assure that a test facility is producing valid emissions data. Approximately 53 persons attended the symposium and are listed in Appendix 1.

The symposium was conducted in the manner of the previous meetings in that informal comments and presentations were encouraged. Because of this spontaneity, it is difficult to record a synopsis that flows with continuity.

The viewgraphs used in the presentations and additional information are contained in the appendices.

## SYNOPSIS OF SYMPOSIUM:

The discussion of the presentations will follow the general outline of the symposium. Agenda Items I, II, and III have been combined because of their similarities.

### Ford

Bruce Gardner, of Ford, presented a summary of quality control checks performed on the test cell equipment. The majority of Ford CVS systems are the venturi type. A list outlining the actual quality checks, the techniques, frequencies, and limits, is shown in Appendix 2.

### Chrysler

Frank Johnson, of Chrysler, presented the quality control checks performed on the test cell equipment. The Chrysler facilities are connected to an on-line computer system which contains the analyzer calibration data and has analyzer range sensing capability.

### Chrysler - Carbon Dioxide-Water Interference

A check list (Appendix 3) used by the Highland Park test cell operators each shift was discussed. The Chrysler carbon monoxide analyzers are equipped with pressurized carbon dioxide filter cells and optical filters. Therefore, the response to moist carbon dioxide is checked each shift. The mechanism for performing this test is built into the bag analyzer benches.

Analyzers are spanned at the beginning of each shift on the most sensitive range and are then checked on the two higher ranges; allowable deviations are  $\pm 2\%$  of the full scale range-to-range. Analyzer ranges that are switched during a test are spanned and zeroed. Chrysler believes in a mid-span check when calibrating so that each time an analyzer is spanned, a mid-span check is made. Unadjusted mid span readings must be  $\pm 1$  recorder division. Typical analyzer ranges at the Chrysler Chelsea Proving Grounds are:

<u>HYDROCARBON</u> (ppm Propane)	<u>CO</u> (ppm)	<u>% CO<sub>2</sub></u>	<u>NOx</u> (ppm)
0-250	0-2000	0-4.0%	0-250
0-100	0-500	0-2.5	0-100
0-25	0-100	0-1.0	0-25

### Chrysler - NOx Converter Efficiency

The NOx converter efficiency is checked weekly with a minimum acceptable efficiency of 90%, preferably 95% or better. If the efficiency is less than 95%, corrective action is taken.

### Chrysler - Cell-to-Cell Correlation

On a weekly basis, at the Proving Grounds, a calibration gas standard of approximately 20-50% of the most commonly used range of the analyzers is analyzed at all test sites. The analyzers are spanned with the daily working gases. A deviation of  $\pm 1$  recorder division from the master curve is cause for immediate action; a deviation of  $\pm .5$  divisions initiates an investigation.

At the Highland Park facility, a gas blending station has been installed and connected to the central calibration system (Appendix 3). The blended gas is available to the cell operator at any time for a check of the analyzers. The system blends two cylinders in a ratio of approximately 20% Cylinder A to 80% Cylinder B. A system has been incorporated in the bag analyzer benches (Appendix 3) so that the blended gas can be read directly or the blended gas can be put in the CVS bags and read from the bags. This enables the operator to:

1. Check the bag analyzer curves.
2. Check the integrity of the CVS bags.
3. Check the bag analyzer sample system.
4. Check the adequacy of the bag evacuation and purge system.
5. Check NOx converter efficiency.

This system was in a trial status at the present time but a sample of the data generated was discussed (Appendix).

Chrysler uses the Heath PDP Constant Volume Sampler with the primary calibration performed using a Meriam Laminar Flow Element. A typical calibration was shown (Appendix).

The Constant Volume Samplers sample integrity is checked daily using a Critical Flow Orifice and propane gas. Typical data are shown (Appendix). If the percent error is greater than  $\pm 2\%$  the cell is shut down and the cause of the disagreement is located. In some instances this requires a CVS recalibration. Propane is used instead of carbon monoxide because of the danger of using 100% carbon monoxide.

Chrysler uses Hydrogen-Helium for the FID fuel instead of hydrogen-nitrogen. Chrysler has used this blend and believes this gives the correct hydrocarbon value, recognizing that this fuel will result in a 3% higher reading than the hydrogen-nitrogen fuel.

General comments on the Chrysler central calibration system were made. The forty-one stainless steel lines were freon flushed and if the system has been static for awhile, the NOx lines are run until a steady calibration value is obtained.

#### EPA

Don Paulsell made the presentation for EPA. Don described the Sample Analysis Correlation (SAC) Program in which a blended gas is placed in a bag and read on all the light duty analyzer sites. The gas is blended using the system shown in Appendix 5. Control limits and control chart flags were discussed and are listed in the Appendix.

The capabilities of the SAC Program include the assessment of site-to-site, range-to-range correlation and repeatability plus the diagnosis of instrument problems. A complete listing of the program capabilities is contained in the Appendix.

Don described EPA's analyzer calibration philosophy, emphasizing that overlapping cal gases are important to ensure range-to-range continuity, and that this practice helps to pinpoint standards that are deteriorating. A common manifold for span gases eliminates the variability of calibration span gases from site-to-site. EPA performs a span check/mid-span check and a quarter-span check during calibration. A summary of the above is contained in the Appendix.

Current EPA analyzer ranges are:

<u>HC (ppm C<sub>3</sub>H<sub>8</sub>)</u>	<u>LCO (ppm)</u>	<u>HCO (ppm)</u>	<u>CO<sub>2</sub> %</u>	<u>NOx (ppm)</u>
0-250	0-1000	0-5000	0-5.0	0-250
0-100	0-500	0-2500	0-2.5	0-100
0-50	0-250		0-1.0	0-50
	0-100			

#### EPA - NOx Converter Efficiency

The NOx converter efficiency is performed once a week. Although 90% is the corrective action limit, typical values are 98%. A mixture of 1% oxygen in Argon was discussed as a potential ozone source to decrease the sensitivity of the ozonator. A mixer is located in the efficiency checker to ensure a uniform gas.

### EPA - Carbon Dioxide-Water Interference

The carbon dioxide and water response on the carbon monoxide analyzers is checked every six months. A typical result of .5 ppm response is experienced, with less than 3 ppm being the maximum allowable response. A Hopcalite (MSA product) scrubber is used to remove the carbon monoxide from the zero air zero gas (Appendix).

### EPA - Tracer Gas Injections

Propane injections are performed weekly using the Critical Flow Orifice technique.<sup>3</sup> Don explained that the density of pure propane is 52.72 gms/ft<sup>3</sup> at 68°F and 1 atmosphere whereas diluted propane is 51.88 gms/ft<sup>3</sup>. EPA is installing CFO manifold systems using the orifices supplied by Turner Corp. A copy of this information is in the Appendix. EPA has determined that the proper equation to use with a CFO kit is:

$$(\text{SCFM}) \quad q = (AP^2 + C) / \sqrt{T_{\text{abs}}}$$

Bomb mass testing is also used at EPA, generally in conjunction with evaporative SHED's (Appendix).

### EPA - CVS Systems

Don described the procedure used by EPA in calibrating the PDP and CFV type sampler systems. The equations and plots used can be found in the Appendix. EPA uses a LFE and collects eight data points per calibration with a tolerance of  $\pm 1\%$  of the curve as acceptable data. EPA does not calibrate through the heat exchanger as Chrysler does. A discussion concerning the traceability to NBS of the Meriam Laminar Flow Elements followed. EPA has sent LFE units to Colorado Engineering Experiment Station, Inc., for recalibration. Copies of typical calibration data are included in the Appendix. The question of how well the calibration supplied by Meriam and a recalibration by the Colorado Engineering Experiment Station, Inc., performed on a new unit agreed was asked. No one present had ever had a new unit recalibrated; only units having prior use had been recalibrated. It was stated that the new units received from Meriam have a calibration traceable to NBS.

### GM - Cell-to-Cell Correlation

Mike Briggs explained the technique used by GM to cross check their bag sites. Weekly, a bag of high concentration and a bag of low concentration exhaust emissions are generated using a vehicle and CVS. The bags are initially checked on a reference site, and then analyzed on each cell, operating or not. The reference cell is changed each week. In order to correct for

nitric oxide decay, the bags are read periodically on the reference cell during the testing of the other cells. A statistical analysis is made to identify outliers outside of two sigma. Hydrocarbon results will differ and the relative response of the FID is suspected. A GC analysis is also performed on the bag. Mike stated that the mid-span on all bag ranges is checked once daily and must be within  $\pm$  2% of the value of the gas.

A zero and span check is performed per each bag group and must be  $\pm$  0.2 MV in the pretest and  $\pm$  1.0 MV in the post-test check. A digital voltmeter and recorder are used in the test cells.

#### GM - NO<sub>x</sub> Converter Efficiency

The NO<sub>x</sub> converter efficiency is checked daily on the most sensitive range of the analyzer and in accordance with the Federal Register test procedure. The minimum acceptable limit at GM is 98% efficiency. A leak check is performed in conjunction with the efficiency check. Carbon dioxide and water vapor interference on the carbon monoxide analyzers are checked each month. Analyzers must meet the Federal Register specifications.

Additional monthly checks include bag analyzer curves, NDIR optimization, and the FID methane response to approximately 60 ppm methane-air mixture. An equivalent factor of 1.12  $\pm$  .02 to C<sub>3</sub>H<sub>8</sub> is typical.

#### GM - CVS System

Tom Slaughter discussed the CVS systems. The GM systems are the Positive Displacement Pump type and are connected to a data acquisition computer. The make-up air supplied to the CVS is provided by an external air supply. Many questions were asked concerning the make-up air and the system used for controlling the humidity, etc.

#### GM - CVS Calibration

A daily propane injection is run on the CVS system using the CFO technique. A  $\pm$  2% agreement is required. GM uses the real gas density of propane and assumes the purity to be 100%. The initial calibration is performed using a LFE on the CVS outlet. GM plans to use a Smooth Approach Orifice instead of the LFE for calibrating the CVS systems because the LFE system calibration changes as the unit gets contaminated.

Agenda Items IV, V, VI, and VII are presented individually as follows:

#### IV. Dynamometer Systems

##### Chrysler

Chrysler uses the Clayton, direct drive, variable inertia flywheel and automatic roadload control equipped dynamometers. The dynamometers are operated in the automatic roadload mode with additional control pots added to the initial system to enable the use of the automatic roadload feature on non-standard horsepower settings. In some instances, the dynamometers are operated in the manual mode. Chrysler is planning to add 125 lb. increment inertia weight capability, dial-a-horsepower thumbwheels, and digital speed and horsepower meters to the existing dynamometers. Distance measurement equipment has recently been added to the dynamometers. The dynamometers are calibrated every thirty days.

The roadload horsepower is checked each test as is the speed calibration of the driver's aids. The inertia weight engagement is verified by the test cell operator before the test. A quick coastdown technique has been used by Chrysler to spot check the dynamometer horsepower calibrations. This technique can be performed after the dynamometer warm-up. It requires that the same vehicle be used and instead of lifting the vehicle from the dynamometer, the coast time is recorded while the vehicle remains on the dynamometer. This technique is quick and provides immediate results when the test site is equipped with an on-line data acquisition system.

The roller spacing on all of the dynamometers is 17.25 inches, except for three truck dynamometers, which have a 20.00 inch spacing.

##### Ford

Ford uses Clayton, direct drive, variable inertia flywheel, roadload control dynamometers with 17.25 inch spacing. The dynamometers are currently operated in the automatic roadload mode. Weekly frictional horsepower and roadload horsepower determinations are performed using the Federal coastdown procedure. Ford has a special vehicle equipped with built in lifts that reduces the amount of time required to perform coastdowns. The driver's aid is checked daily by comparing the number of dynamometer roller revolutions vs. the time at a specific speed with an allowable tolerance of  $\pm 0.1\%$ . The tach generator voltage versus speed calibration is checked bi-monthly using a digital counter with a tolerance of  $\pm 10$  rpm of the set point.

GM

GM uses the Clayton direct drive, automatic roadload control dynamometers with 17.25 inch roller spacing. The dynamometers are operated in the automatic roadload control mode. The Clayton dynamometers electronics have been modified to provide thumbwheel horsepower selection capability. Further modifications have been made as explained in EPA/Industry Symposium #1.

GM uses a computerized program utilizing the least squares linear curve fit to generate the indicated horsepower versus the actual horsepower data.

The dynamometer rollers have been machined to give a uniform roller circumference and solid bearing supports have been employed. The dynamometers have been aligned using a laser beam.

A full dynamometer speed and horsepower verification is performed every thirty days using a special coastdown vehicle. The speed is calibrated using a line synchronized stroboscope. A horsepower check is performed before and after each test.

EPA

EPA uses the Clayton direct drive variable inertia fly-wheel, automatic roadload control dynamometers with 17.25 inch roller spacing. EPA operates in the automatic roadload mode. A chart showing the statistics for the distance traveled during the various phases of the FTP and HWFE cycle was discussed. The chart is contained in the Appendix. A brief summary is:

FTP (812 tests)

Cold transient	-	3.6058 mi.
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Cold stabilized	-	3.9010 mi.
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Hot transient	-	3.6067 mi.
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<u>HWFE (691 tests)</u>	-	10.295 mi.
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The rear roller revolutions are monitored using an encoder that gives 320 pulses per revolution, which are totaled at 10/rev.

The EPA calibration techniques and supporting data are contained in detail in the EPA/Industry Symposium #1 proceedings.

## V. Total System Checks

Ford uses the exhaust flow simulator daily for a total system check. The simulator uses critical orifices to inject known amounts of emissions components.

Chrysler uses a correlation vehicle on a weekly basis to cross check the total system of each cell. A hot 505 cycle is run using the running start technique. The vehicle oil and water temperatures are stabilized using a 40 mph steady state prior to the test. On a monthly basis vehicles are switched from the Proving Grounds and Highland Park for a facility-to-facility comparison.

The correlation limits are:

	<u>HC</u>	<u>CO</u>	<u>NOx</u>	<u>CO<sub>2</sub></u>
Gms/Mi.	1.40	8.5	3.3	600
% Variation	5.0	10.0	8.0	3.0
	<u>HC</u>	<u>CO</u>	<u>NOx</u>	<u>CO<sub>2</sub></u>
Gms/Mi.	0.5	4.0	2.3	670
% Variation	10.0	15.0	10.0	3.0

Typical data are contained in the appendix.

GM checks each site every day using a vehicle and evaluates the data statistically using a two week moving average. If a cell has two successive CO<sub>2</sub>/NOx readings that are outliers, the dynamometer is checked.

VW stated that an automatic driver reduces data variation on cell-to-cell total systems checks.

Dick Lawrence, of EPA, discussed the effect that the calibration of the thermometers can have on the KH factor. If a facility is using a wet and dry bulb apparatus using mercury thermometers that are not matched, an error can be introduced that will have a significant effect on the KH factor. He further stated that EPA intends to purchase a dewpoint instrument for evaluation.

Don Paulsell stated that an effective cell correlation program should have both small (2000 lb. inertia) and a large (4000 lb. inertia) vehicle involved in the program.

## VI. SHED

Chrysler has 3 SHED's at the Proving Grounds, one AESI and two Eller, equipped with internal and external cooling. The AESI is 10' x 8' x 21' with a total volume of 1680 ft.<sup>3</sup> and the Ellers are 10' x 10' x 24' with a total volume of 2400 ft.<sup>3</sup>.

GM Proving Grounds has six SHED's, five with a volume of 1850 ft.<sup>3</sup> and one with a volume of 2560 ft.<sup>3</sup>. The systems were designed by the MVEL. A list of the details is contained in the Appendix.

## VII. State-of-the-Art Diagnostic Techniques

Everyone involved in emissions testing is striving to develop quality control monitoring techniques that can be performed during the course of the testing. The amount of non-productive time expended in performing the necessary quality control checks can be reduced, while at the same time providing the assurance that a facility is producing valid data.

Don Paulsell discussed some of the EPA techniques that are part of the data processing program for the FTP and HWFE tests. A list of these parameters and the limits used to assess abnormal data are shown in the Appendix.

## A G E N D A

### EPA/INDUSTRY QUALITY CONTROL SYMPOSIUM INTRA-LABORATORY TEST SITE/EQUIPMENT QUALITY CONTROL TECHNIQUES

October 5, 1977  
9:00 A.M. - 4:00 P.M.

#### I. Bag Analyzer

- . Cell-to-Cell Correlation
- . Daily Calibration - Range to Range Span Checks
- . NO<sub>x</sub> Converter Efficiency Check
- . Water and Carbon Dioxide Interference Checks

#### II. CVS Systems

- . Description of the CVS Systems
- . Method of Primary Calibration

#### III. CVS Systems Sample Integrity

- . Tracer Gas - Propane Injection
- . Bag Leak Checks
- . System Leak Checks
- . Hydrocarbon Hangup

- LUNCH 11:30 A.M. - 12:30 P.M. -

#### IV. Dynamometer System

- . Driver's Aid Calibration
- . Roller Revolution Monitoring - Distance Measurement Equipment
- . Speed Check
- . Roadload Horsepower Check
- . Frictional Horsepower Check
- . Inertia Weight Monitoring and Horsepower Monitoring During Test

#### V. Total System Checks

- . Correlation Vehicles
- . Mass Flow Simulator
- . Analysis Techniques - BREAK - 15 MINUTES -

#### VI. SHED

- . Calibration
- . Leak Check
- . Propane Retention
- . Temperature Monitoring
- . Background Check

#### VII. State of the Art Diagnostic Techniques

- . Shortcomings of Present Methods
- . Productive (during the test) Techniques for Quality Control
- . Special Equipment

APPENDIX

1. Attendance List

2. Ford Motor Company

Agenda Item I - Bag Analyzer  
Agenda Item II - CVS Systems  
Agenda Item III - CVS Systems Sample Integrity

3. Chrysler Corporation

Agenda Item I - Bag Analyzer  
Agenda Item II - CVS Systems  
Agenda Item III - CVS Systems Sample Integrity

4. General Motors Corporation

Agenda Item I - Bag Analyzer  
Agenda Item II - CVS Systems  
Agenda Item III - CVS Systems Sample Integrity

5. Environmental Protection Agency

Agenda Item I - Bag Analyzer  
Agenda Item II - CVS Systems  
Agenda Item III - CVS Systems Sample Integrity

6. Agenda Item IV - Dynamometer System

- a. Ford Motor Company
- b. Chrysler Corporation
- c. General Motors Corporation
- d. Environmental Protection Agency

7. Agenda Item V - Total System Checks

- a. Chrysler Corporation
- b. Environmental Protection Agency

8. Effect of Accuracy of Wet and Dry Bulb Measurement  
on Kh Factor

9. Agenda Item VI - SHED

- a. Ford Motor Company
- b. General Motors Corporation

10. EPA In-Process Quality Control Techniques

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Name: R. E. Martin  
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Telephone: (312) 339-3300, Ext. 519

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A T T E N D A N C E   R O S T E R

EPA/INDUSTRY QUALITY CONTROL SYMPOSIUM  
INTRA-LABORATORY TEST SITE/EQUIPMENT  
QUALITY CONTROL TECHNIQUES

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October 5, 1977  
9:00 A.M. - 4:00 P.M.

---

Name: John D. Harrod  
Company: Cummins Engine Co., Inc.  
Address: 1900 McKinley Ave., Columbus, Indiana 47201  
Telephone: (812) 379-5335

---

Name: J. M. Trapp  
Company: Cummins Engine Co., Inc.  
Address: 1900 Mc Kinley Ave., Columbus, Indiana 47201  
Telephone: (812) 379-5335

---

Name: Steve Whittier  
Company: Ford Motor Co., Scientific Research Laboratory  
Room E-2212  
Address: 21500 Oakwood Blvd., Dearborn, Mich. 48121  
Telephone: (313) 323-3301

---

Name: Geoffrey R. Jones  
Company: Ford Motor Company, Emissions Test Lab.  
Address: 1500 Enterprise Drive, Allen Park, Mich. 48121  
Telephone: (313) 322-3458

---

Name: Daniel A. Reis  
Company: Jeep Corp.  
Address: 940 N. Cove Blvd., Toledo, Ohio  
Telephone: (419) 470-7453

---

Name: Phillip Ingram  
Company: General Motors Proving Grounds (V.E.L.)  
Address: Milford, Michigan  
Telephone: (313) 685-6376

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A T T E N D A N C E      R O S T E R

EPA/INDUSTRY    QUALITY CONTROL SYMPOSIUM  
INTRA-LABORATORY TEST SITE/EQUIPMENT  
QUALITY CONTROL TECHNIQUES

October 5, 1977  
9:00 A.M. - 4:00 P.M.

---

Name:        E. H. Howell  
Company:     International Harvester Co.  
Address:     2911 Meyer Road, Ft. Wayne, Ind.  
Telephone:

---

Name:        Bruno Rapetti  
Company:     Fiat - Italy  
Address:     Str. Del Drosso 145, Torino, Italy  
Telephone:

---

Name:        Wolfgang Groth  
Company:     Volkswagen of America  
Address:     818 Sylvan Ave, Englewood Cliffs, N. J. 07632  
Telephone:

---

Name:        Daniel R. Wamboldt  
Company:     American Motors Corp.  
Address:     5626 - 25th Ave.  
Telephone:   Kenosha, Wis. 53140

---

Name:        Frank E. Johnson  
Company:     Chrysler Corporation  
Address:     P. O. Box 1118, Detroit, Mich. 48288  
Telephone:   (313) 956-3135

---

Name:  
Company:  
Address:  
Telephone:

MISCELLANEOUS

<u>QC CHECK</u>	<u>TECHNIQUE</u>	<u>FREQUENCY</u>	<u>ACCURACY</u>
1. Wet/Dry Psychrometer	Sling Psychrometer	Daily	$\pm$ 5 grains H <sub>2</sub> O/lb air
2. <u>Test Cell</u> Vacuum Gauge	Mercury Manometer	6 Months	$\pm$ .5 in Hg
3. Barometer Calibration	Mercury Barometer	Monthly	$\pm$ .01 in Hg

CVS/ANALYZER SYSTEM

<u>QC CHECK</u>	<u>TECHNIQUE</u>	<u>FREQUENCY</u>	<u>ACCURACY</u>
1. Analyzer Calibration	Gas Bottle	30 Days	$\pm 1\%$
2. NOx Converter Efficiency	per Fed. Reg.	7 Days	97%
3. CVS Flow Calibration	LFE	6 Months	$\pm .05$ const.
4. CVS Timers	Stopwatch-3 min.	30 Days	$\pm 1$ sec.
5. CVS Verification	Mini-propane or gravimetric	30 Days	$\pm 2\%$
6. CVS Temperature Recorder Calibration	Resistance	6 Months	$\pm 1^{\circ}\text{F}$
7. CVS/Analyzer System	Exhaust gas simulator	Daily	$\pm 5\%$

24

COPY NUMBER= 2

CHRYSLER CORPORATION EMISSION DEVELOPMENT TESTING  
BLOWER CALIBRATION PROGRAM

\*\*\*\*\*

CVS-MEATH 22 0

\*\*\*\*\*

LIBRATION PERFORMED ON-3/02/77 BY DOWNEY  
OVER SPEED NUMBER THREE

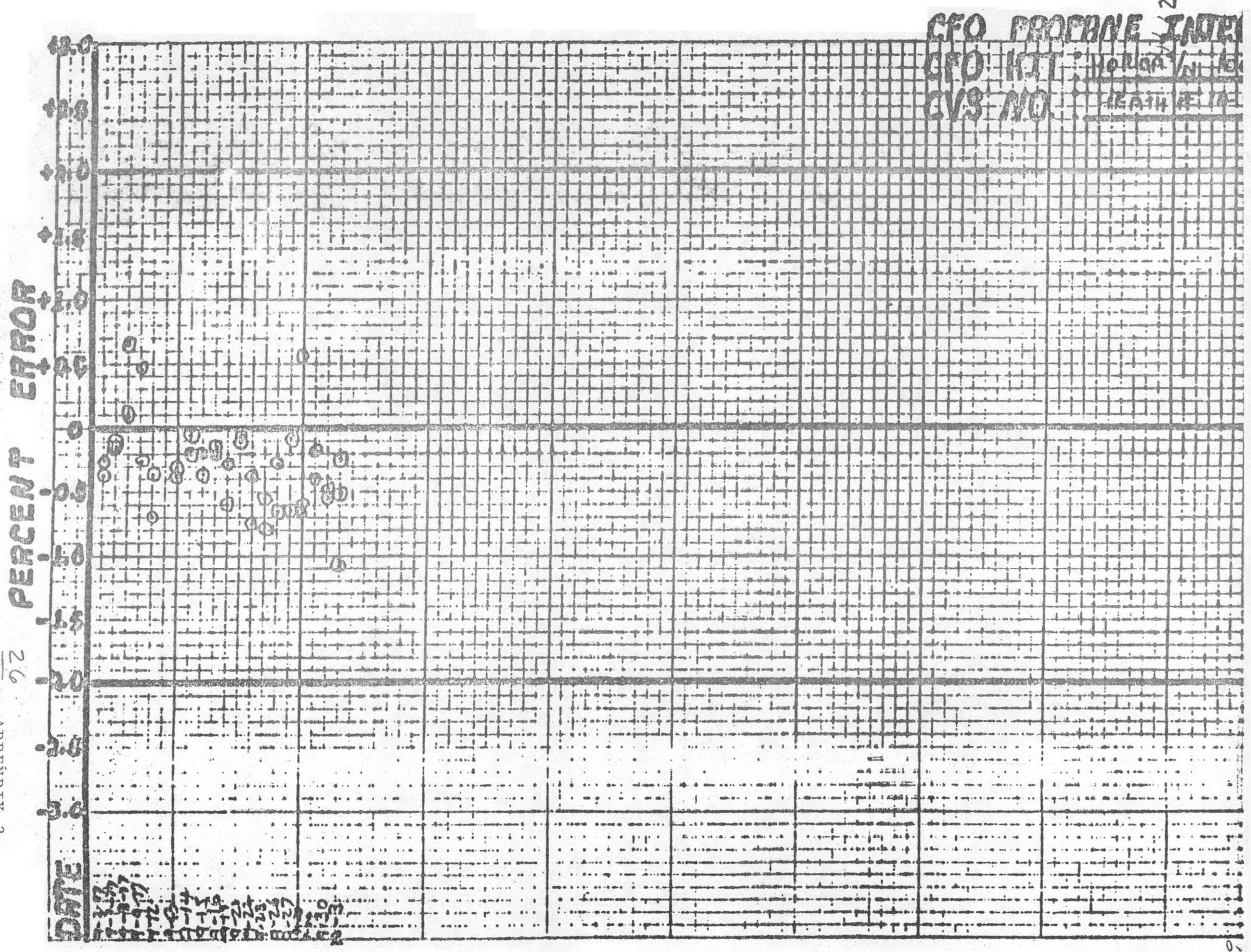
THE LFE USED WAS-F33221R1

IS IFF HAS A SLOPE OF 194.47 AND AN INTERCEPT OF 6.74  
IE ELEMENT WAS MOUNTED BEFORE THE CVS

IS RECALIBRATION WITH A3c8 BLOWER HR30

BLOWER DELTA P	PUMP RPM	CFM	CF/REV
15	1355.0	417.0	.3075
16	1354.0	415.6	.3067
17	1354.2	414.3	.3059
18	1353.3	413.0	.3052
19	1352.4	411.7	.3044
20	1351.4	410.4	.3037
21	1350.7	409.2	.3030
22	1349.9	408.0	.3023
23	1349.0	406.8	.3016
24	1348.1	405.7	.3009
25	1347.3	404.6	.3003
26	1346.4	403.4	.2996
27	1345.6	402.3	.2990
28	1344.7	401.2	.2984
29	1343.8	400.2	.2978
30	1343.0	399.1	.2972
31	1342.1	398.1	.2966
32	1341.2	397.1	.2960
33	1340.4	396.0	.2953
34	1339.5	395.0	.2949
35	1338.7	394.1	.2944
36	1337.8	393.1	.2938
37	1336.9	392.1	.2933
38	1336.1	391.2	.2928
39	1335.2	390.2	.2922
40	1334.4	389.3	.2917

12  
CFO PROPANE INTE  
CFO INT. NO. 10  
CVS NO. 10



INSTRUMENTATION VERIFICATION  
CVS PROPANE INJECTION V/CPO  
CHELSEA PROVING GROUNDS  
DEPARTMENT 5150  
VEHICLE CERTIFICATION

DATE: 10-4-77

<u>CELL NUMBER</u>	<u>CVS NUMBER</u>	<u>AVERAGE % ERROR*</u>	<u>ENGINEER</u>
1	MEATH 12	-1.1 / -0.9	NP
2	" 13	0.6 / 0.4	JB
3	" 10	0.5 / 0.8	NP
4	" 14	-0.8 / -1.3	NP
5	" 9	-0.4 / -0.8	JB
6	" 29	-0.3 / -0.4	NP
7	" 11	-1.0 / -1.4	NP
8	" 15	1.0 / 0.4	NP

\* Positive errors may be due to:

1) A decrease in:

- a) Cubic feet per revolution (CVS flow rate)
- b) Inlet temperature
- c) Background concentration

2) An increase in:

- a) Pump clearance
- b) Inlet pressure
- c) Barometric pressure
- d) Revolution counter
- e) Spent gases

\* Negative errors may be due to the opposite of each of the above positive errors,  
or to a leak in the CVS or analytical system.

COMMENTS: Any deviations  $> \pm 2\%$  must be resolved before  
the CVS may be used for testing.

Calc.:  $\frac{[CVS] - [CFO]}{[CFO]} \times 100 = \text{_____ \% Error}$

**ROLLS OPERATORS DAILY CHECK LIST**

DATE: 10-3-77 SERIAL: 1 ROLLS: 23 OPERATOR: H. P. SORENSEN

## **LEAK CHECKS**

T.P. BENCH	✓
CO <sub>2</sub> DILUTE	✓
CO <sub>2</sub> EGR	✓
ENG. BENCH	✓
BAG BENCH	✓
7.S. SAMPLE SYS.	✓
BAG #1	✓
BAG #2	✓
BAG #3	✓
BAG #4	✓
BAG #5	✓
BAG #6	✓

**TUNE-GAIN PRESSURE CHECK**

	<u>TUNE</u>	<u>GAIN</u>	<u>SAMP. P.</u>	<u>O<sub>2</sub> P.</u>	<u>H<sub>2</sub> P.</u>	<u>Z. AIR P.</u>
BAG BENCH						
CO	<u>43.1</u>	<u>418</u>	<u>X</u>	<u>X</u>	<u>X</u>	<u>X</u>
CO <sub>2</sub>	<u>36.0</u>	<u>800</u>	<u>X</u>	<u>X</u>	<u>X</u>	<u>X</u>
NOX	<u>X</u>	<u>X</u>	<u>4.0</u>	<u>20.0</u>	<u>X</u>	<u>X</u>
EC	<u>X</u>	<u>X</u>	<u>1.5</u>	<u>X</u>	<u>25.0</u>	<u>20.0</u>
T.P. BENCH						
LO CO	<u>34.1</u>	<u>448</u>	<u>X</u>	<u>X</u>	<u>X</u>	<u>X</u>
H CO	<u>35.0</u>	<u>200</u>	<u>X</u>	<u>X</u>	<u>X</u>	<u>X</u>
CO <sub>2</sub>	<u>41.8</u>	<u>620</u>	<u>X</u>	<u>X</u>	<u>X</u>	<u>X</u>
CO <sub>2</sub> DILUTE	<u>34.1</u>	<u>250</u>	<u>X</u>	<u>X</u>	<u>X</u>	<u>X</u>
CO <sub>2</sub> EGR	<u>38.3</u>	<u>500</u>	<u>X</u>	<u>X</u>	<u>X</u>	<u>X</u>
NO	<u>X</u>	<u>X</u>	<u>4.0</u>	<u>20.0</u>	<u>X</u>	<u>X</u>
EC	<u>X</u>	<u>X</u>	<u>1.5</u>	<u>X</u>	<u>25.0</u>	<u>25.0</u>
ENG. BENCH						
LO CO	<u>40.0</u>	<u>634</u>	<u>X</u>	<u>X</u>	<u>X</u>	<u>X</u>
H CO	<u>40.0</u>	<u>750</u>	<u>X</u>	<u>X</u>	<u>X</u>	<u>X</u>
CO <sub>2</sub>	<u>37.0</u>	<u>700</u>	<u>X</u>	<u>X</u>	<u>X</u>	<u>X</u>
NO	<u>X</u>	<u>X</u>	<u>4.0</u>	<u>20.0</u>	<u>X</u>	<u>X</u>
EC	<u>X</u>	<u>X</u>	<u>1.5</u>	<u>X</u>	<u>25.0</u>	<u>25.0</u>

### C.V.S. PARAMETERS

METER PCS  
98 97  
11.4 11.5  
21.9 21.9

**CO<sub>2</sub>-H<sub>2</sub>O INTERFERENCE CHECK**

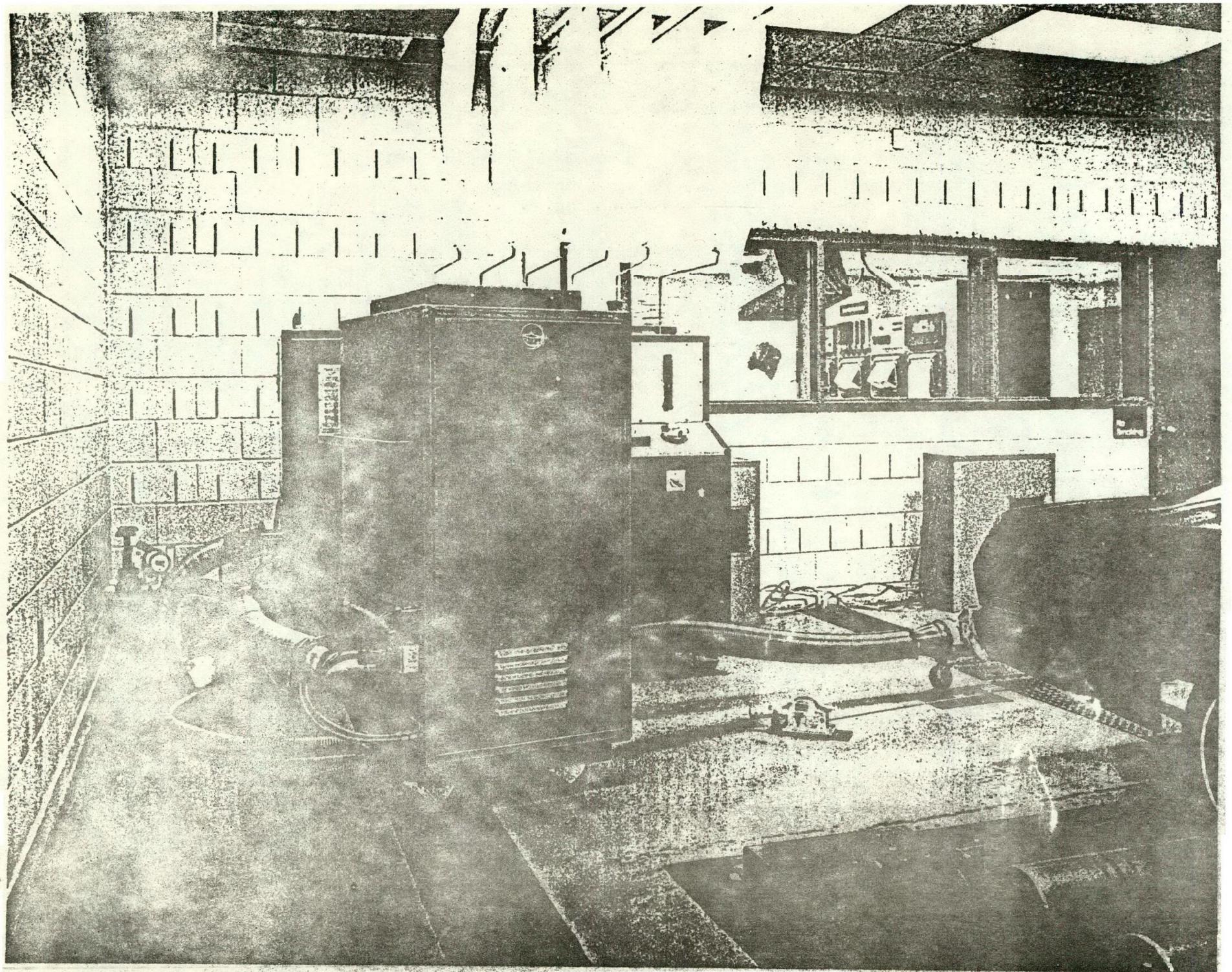
RANGE: LII ZERO	0.0
DRY CO <sub>2</sub> RESPONSE	1.2
WET CO <sub>2</sub> RESPONSE	1.7

**BY-PASS FLOW RATE CHECK**

T.P. BENCE  
CO<sub>2</sub> DILUTE  
CO<sub>2</sub> EGR  
ENG. BENCE

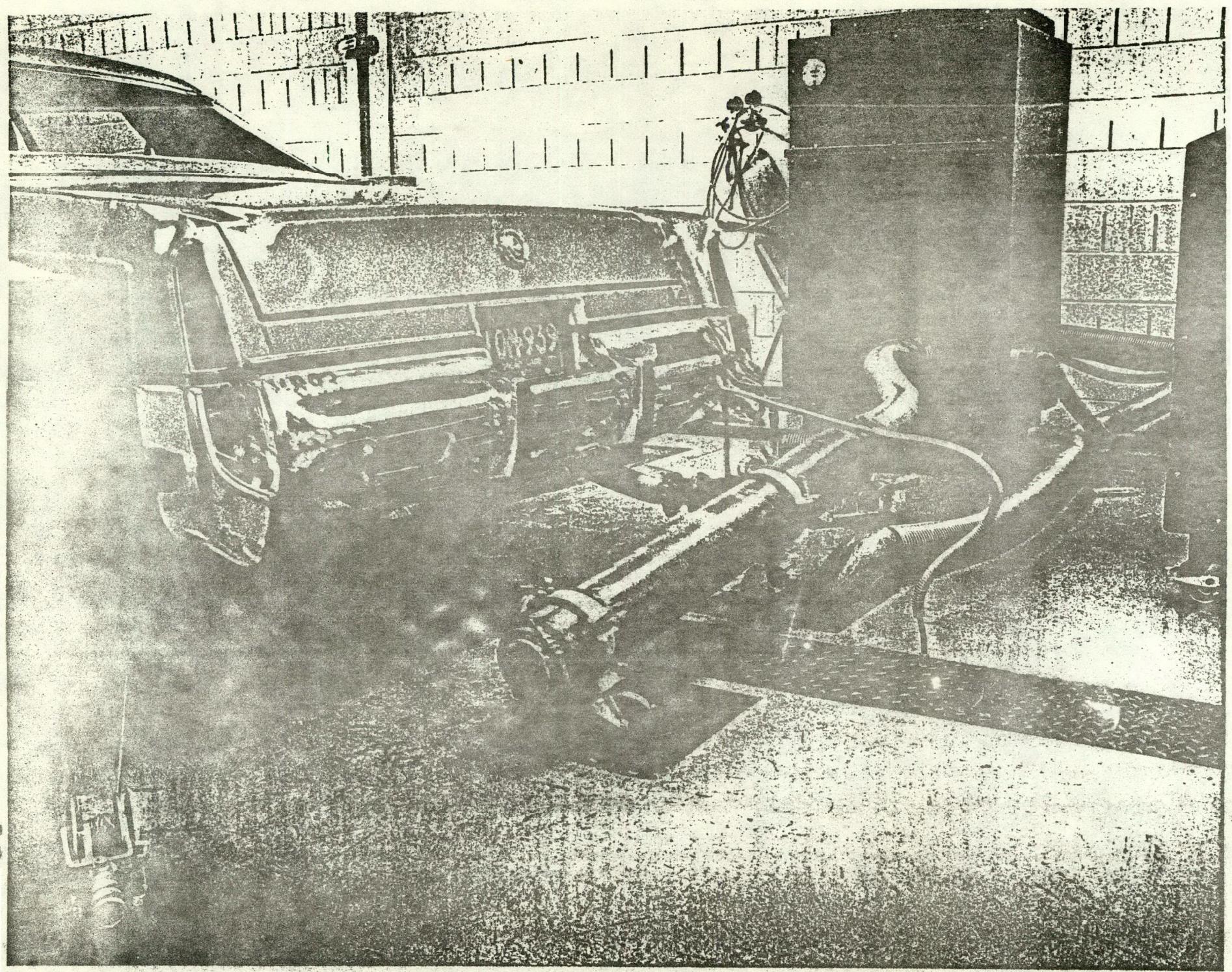
5140/EPS

28



F. Johnson CH

APPENDIX 3



- 540

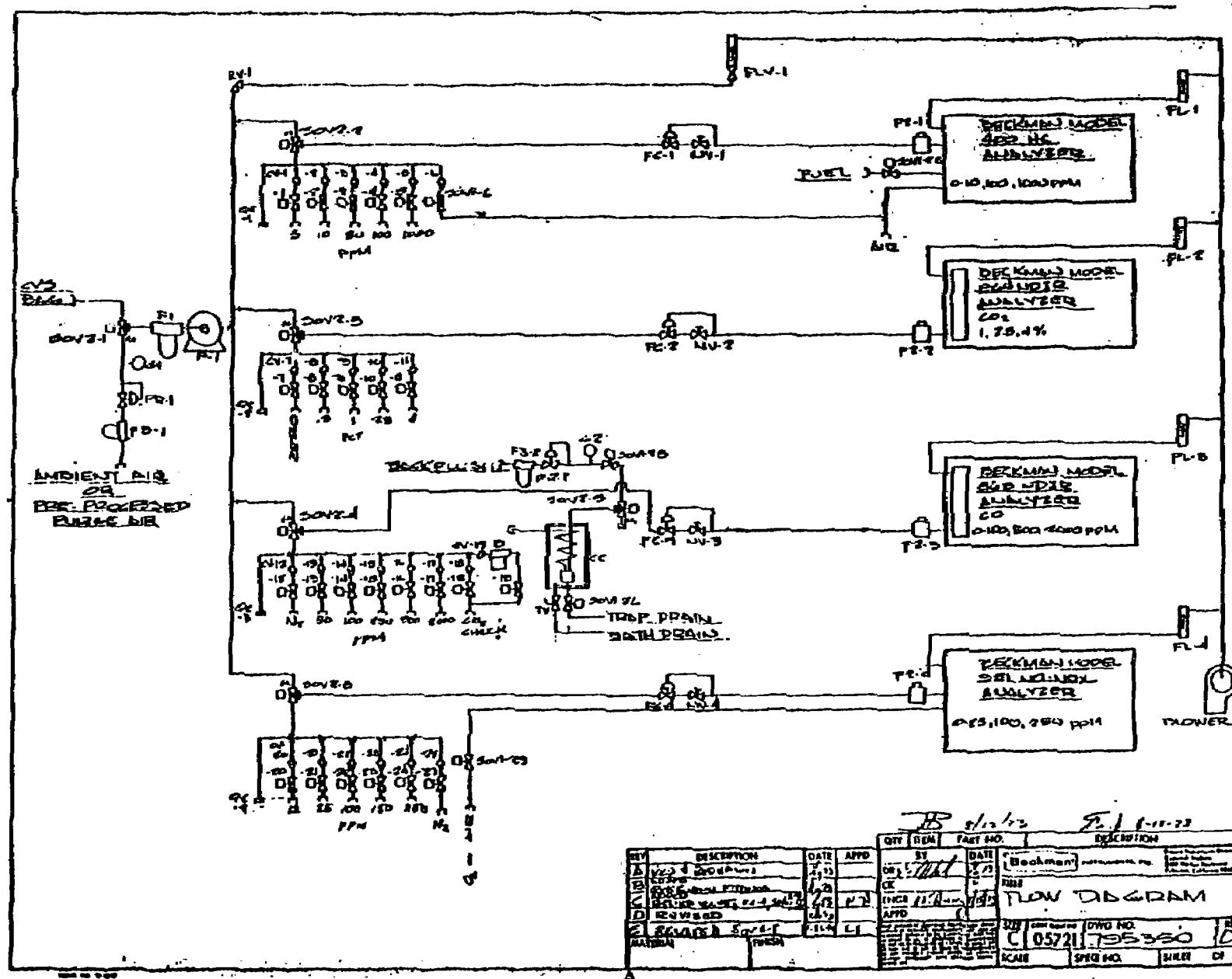
3 VITCINI ET AL.

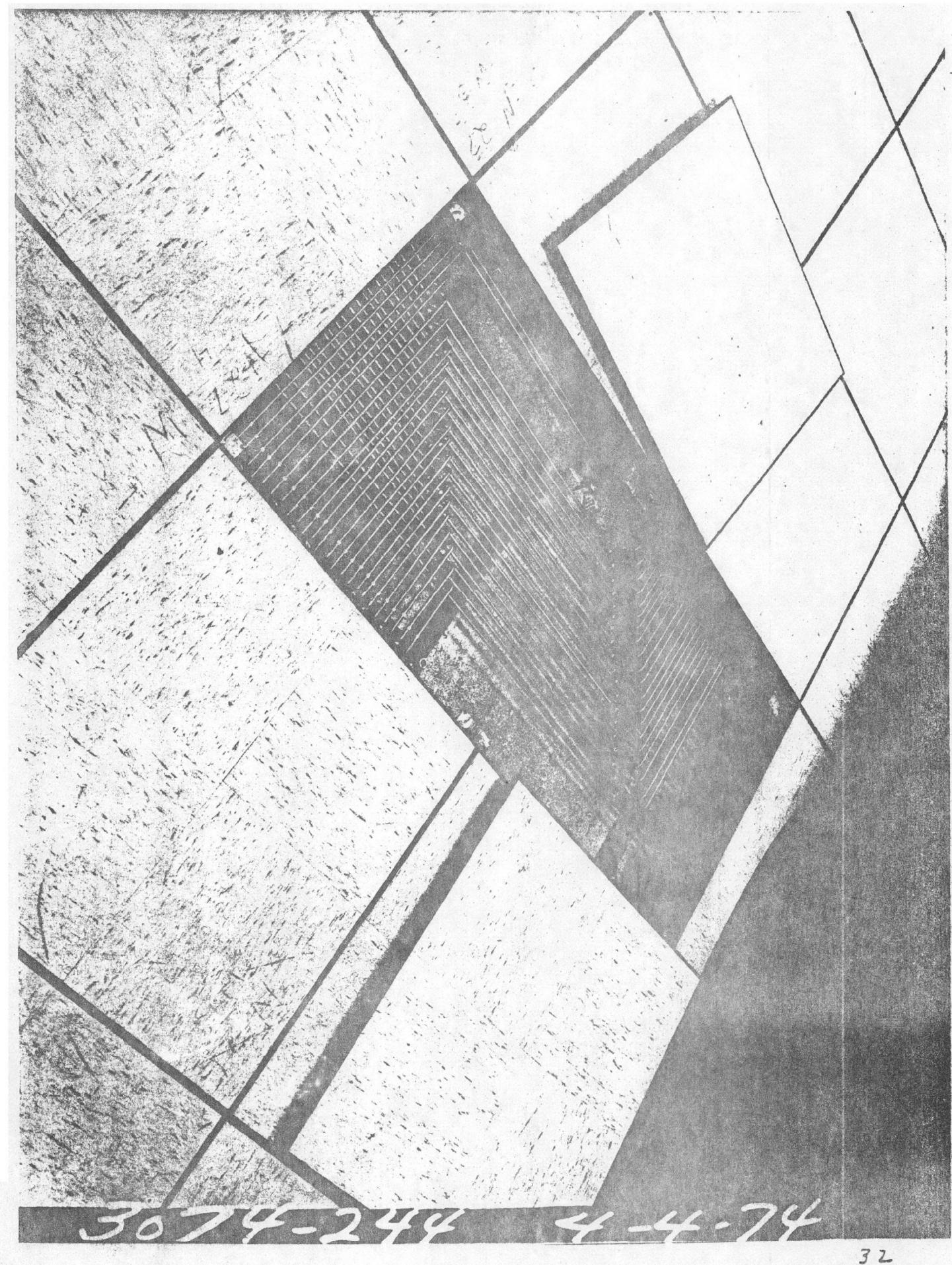
JOHNSON.

CHRYSLER

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Date \_\_\_\_\_ A Rep. \_\_\_\_\_

ISSUE DATE	9-8-77	REV. DATE					
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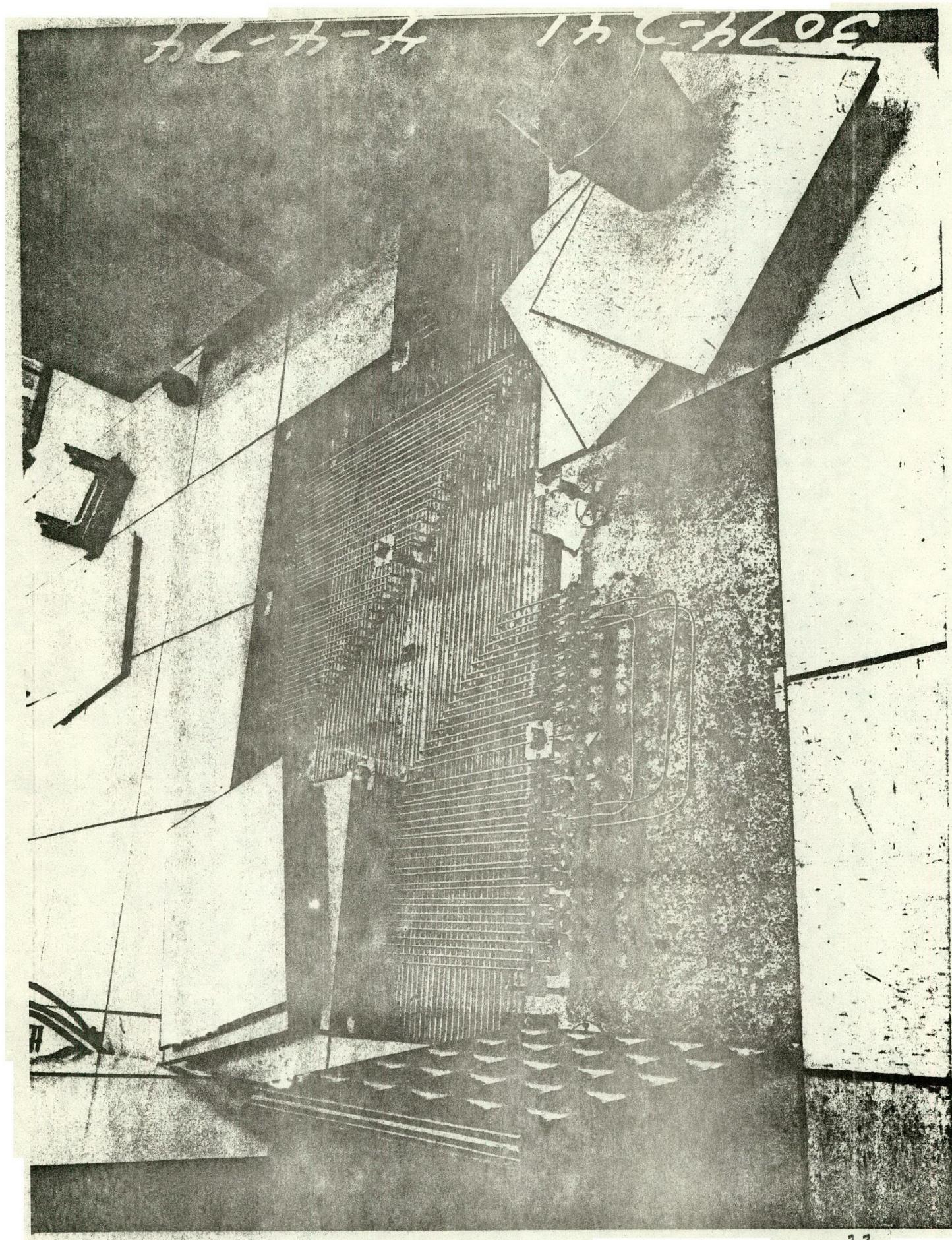


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32

APPENDIX 3

F. Johnson CHRV

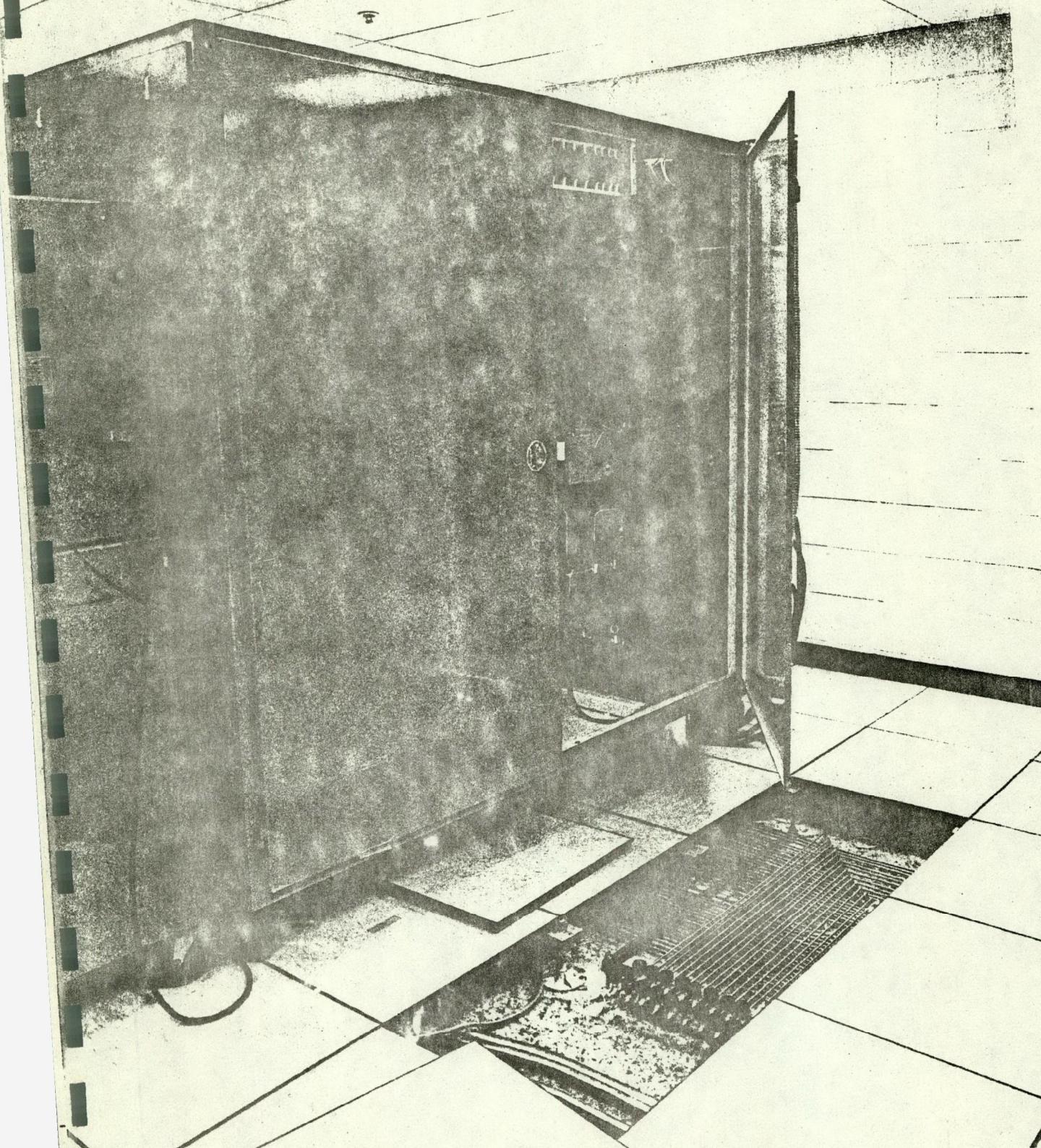


33

AL-AL-AL

E. LALLANAS CHA

カニ-カニ-エキ-カニ



APPENDIX 3

F. JOHNSON (HRV)

34

100 PPM C<sub>3</sub>H<sub>8</sub>

725 PPM CO

9% CO<sub>2</sub>

20% O<sub>2</sub>

BAL. N<sub>2</sub>

32 PPM NO<sub>2</sub>

BAL. N<sub>2</sub>

20% MIX.

80%

BLENDER

CORRELATION CHECK

ANALYZERS & BAG FILL  
(A) OFF (B)

DOUBLE THROW CENTER OFF SWITCH  
MOUNTED ON BAG CART

CALIB GAS  
S LINE 41

CVS BAG

COMPOSITE MIXTURE

20 PPM C<sub>3</sub>H<sub>8</sub>

145 PPM CO

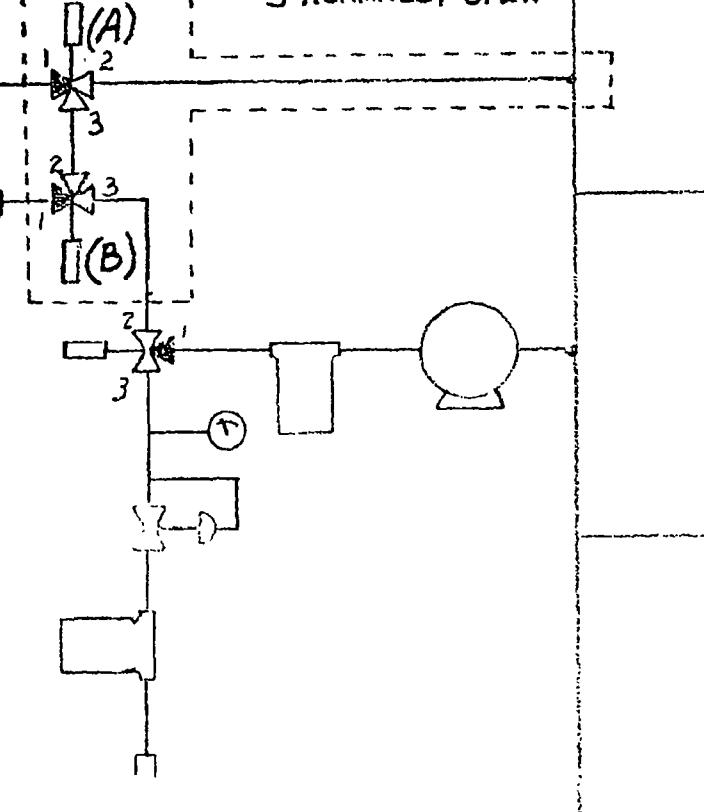
1.8% CO<sub>2</sub>

4% O<sub>2</sub>

BAL. N<sub>2</sub>

BAG CART MODIFICATION

- ✓ 1 COMMON
- 2 NORMALLY CLOSED
- 3 NORMALLY OPEN



TO ANALYZERS

TO READ TEST GAS:

- 1.) ANALYTICAL SYSTEM IN "SAMPLE".
- 2.) SAMPLE PUMP OFF.
- 3.) SWITCH TO "ANALYZERS".

TO READ BAGS:

- 1.) OPCON IN "BAG READ".
- 2.) ANALYTICAL SYSTEM IN "SAMPLE".
- 3.) SAMPLE PUMP ON.
- 4.) SWITCH "OFF".
- 5.) CYCLE OPCON THRU VARIOUS BAGS.

TO FILL BAGS.

- 1.) OPCON IN "BAG READ".
- 2.) SAMPLE PUMP "OFF".
- 3.) SWITCH TO "BAG FILL".
- 4.) CYCLE OPCON THRU VARIOUS BAGS.



# GAS PROPORTIONERS

## MINI-PROPORTIONER®

805-2000 for 2 Gas Mixtures / 805-2001 for 3 Gas Mixtures  
A Portable, Extremely Accurate Gas Mixing System

\$ 250.00

The MINI-PROPORTIONER® is a portable, extremely accurate gas mixing system. Used to blend two or three gases in exact proportions, it is ideal for inert gas welding, atmospheres (forming gas mixtures), generator cooling and other commercial applications.

The MINI-PROPORTIONER® has important features found only in very expensive stationary proportioners. It is a demand type proportioner with built-in mixed gas reservoir and regulator to maintain constant pressure and flow of mixed gas to the work station. High flow capabilities to 200 scfh and a four-station manifold permits up to four operators to use the proportioner simultaneously.

This proportioner is easy to use. Simply connect to gas supply, set supply regulators to 75 psi and the proportioner does the rest. This unit has no electrical requirements, weighs only 30 pounds and can be used anywhere.

### Features

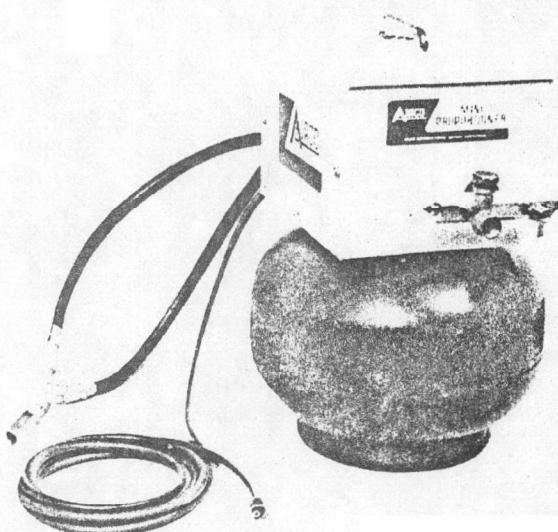
- Extremely accurate  $\pm$  0.5% of exact mixture.
- Each unit is factory set to meet user's requirements.
- Simple to use
- Constant delivery pressure is maintained by a built in regulator. Set at 15 or 30 psig.
- Economical
- Weighs only 30 pounds.
- A unique mechanical cycler precisely controls mixing.
- Demand Proportioner utilizes a mixed gas reservoir with safety relief valve.
- Manifold has 4 outlets.
- High gas flow capability — to 200 scfh.

### Benefits

Accurate gas mixtures for protective welding atmospheres.

Tamper proof — Operator cannot inadvertently change gas mixture.

Minimum set up time



### Versatile

Eliminates the need to buy pre-mixed gas  
Portable — easily carried and used anywhere  
No electrical requirements  
Minimum maintenance — no solenoids to replace  
Safety — Internal pressure protection  
As many as 4 operators can use the MINI-PROPORTIONER® at once.  
For increased capacity two or more MINI-PROPORTIONERS® may be used in parallel.

### Specifications:

#### Inlet Connections:

- Major Gas —  $5/8$ —18 R.H. Internal
- Minor Gas —  $5/8$ —18 R.H. External for CO<sub>2</sub>, argon, helium or nitrogen
- 9/16—18 R.H. Internal for oxygen
- 9/16—18 L.H. Internal for hydrogen

# GAS PROPORTIONERS



## MINI-PROPORTIONER® (continued)

Outlet Manifold has 4 ea.  $\frac{1}{4}$ " N.P.T. Internal Threads

2 Plugged

2 Valves with  $\frac{1}{8}$ -18 R.H.  
Internal Threads

Delivery Pressure 15 or 30 psi (preset).

Inlet Pressure 75-100 psi depends on outlet pressure.

Max Flow 160-400 scfh (most mixtures 200 scfh).

Capable of 2 or 3 gas mixtures in any proportion  
— Gases include argon, CO<sub>2</sub>, oxygen, nitrogen, helium and hydrogen (except for explosive mixtures).

### How To Order

- Specify the stock number of the appropriate proportioner.

Stock no. 805-2000 for mixing 2 gases.

Stock no. 805-2001 for mixing 3 gases.

- Specify the gases to be mixed and the mixture by percent of each gas.

- Specify delivery pressure requirements.

NOTE: The proportioner is factory set to deliver at 15 p.s.i.g. unless otherwise specified.

### Equipment Required for Accurate Control

Regulators — The MINI PROPORTIONER® is calibrated at 75 p.s.i.g. inlet pressure. Two stage regulators with delivery capability of 75 p.s.i.g. are recommended. Airco regulators are listed below:

### Cylinder Regulators

Gas Service	Stock No.	2½" PSI Pressure Gauges	Max. Flow CFH	Max. Work Pressure PSI	Connections		
					CGA No.	Inlet	Outlet
CO <sub>2</sub> *	806-8005	200 & 2000	135	120	320	.830-14 R.H. Int.	"B" $\frac{1}{8}$ -18 R.H. Int.
Argon Nitrogen	806-8420	200 & 4000	975	100	540	.908-14 R.H. Int.	"B" $\frac{1}{8}$ -18 R.H. Int.
Argon Helium Nitrogen	806-9402	200 & 4000	975	100	580	.960-14 R.H. Ext.	"B" $\frac{1}{8}$ -18 R.H. Int.
Nitrogen	806-8427	200 & 4000	975	100	550	.908-14 L.H. Int.	"B" $\frac{1}{8}$ -18 R.H. Int.
Hydrogen	806-9453	200 & 4000	975	100	350	.830-14 L.H. Int.	"B" $\frac{1}{16}$ -18 L.H. Ext.
Oxygen	806-8456	200 & 4000	975	100	540	.908-14 R.H. Int.	"B" $\frac{1}{16}$ -18 R.H. Ext.
Helium	806-9458	200 & 4000	975	100	350	.830-14 L.H. Int.	"B" $\frac{1}{8}$ -18 R.H. Int.

\*806-8005 is an electrically heated CO<sub>2</sub> regulator.

### Flow Control Equipment:

To fully benefit from the economies resulting from proportioning gases, flow control equipment should be used. Airco general purpose (universal) flowmeters are listed for your convenience.

Fixed flow adapters are also available for use where optimum constant flow rates are known.

See ADI 1763 for details.

### Universal Flowmeters

STOCK NO.	DESCRIPTION	FLOW RANGE (S.C.F.H. AIR)	
801-0430	Single Range General Purpose Flowmeter	3-56 @ 15 PSIG	4-68 @ 30 PSIG
805-1606	Dual Range General Purpose Flowmeter	Low Scale	2-23 @ 15 PSIG 2-28 @ 30 PSIG
		High Scale	30-180 @ 15 PSIG 35-220 @ 30 PSIG

C.V.S. SAMPLING SYSTEM CORRELATION  
CRITICAL FLOW BLENDER

WEEK OF 9/19/77

		ROLLS 20	ROLLS 21	ROLLS 22	ROLLS 23	ROLLS 24	ROLLS 25	ROLLS 26	ROLLS 27
SPAN GAS CALIB.	HC	<u>Down</u>	198.5	198.5	198.4	198.3	198.4	198.3	198.5
	CO		1411.7	1410.8	1414.2	1414.4	1409.0	1411.4	1416.4
	CO <sub>2</sub>		3.04	3.04	3.03	3.04	3.04	3.04	3.03
	NOx		207.7	207.7	207.0	207.7	207.5	207.9	207.4
XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX
DIR. FROM BLEND.	HC	<u>Down</u>	167.8	166.4	166.6	166.5	165.6	166.6	166.3
	CO		1958.2	1992.2	1957.6	2003.4	1999.0	2010.2	2031.3
	CO <sub>2</sub>		2.64	2.60	2.61	2.61	2.61	2.62	2.61
	NOx		148.0	148.6	147.3	147.9	145.8	148.7	148.7
XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX
BAG #1	HC	<u>Down</u>	168.2	163.7	167.6	168.0	165.0	165.5	164.1
	CO		1954.3	1990.1	1974.2	1998.3	1987.3	1999.8	2005.6
	CO <sub>2</sub>		2.66	2.60	2.62	2.60	2.61	2.61	2.59
	NOx		150.4	137.7	149.6	154.9	144.3	142.6	145.9
XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX
BAG #2	HC	<u>Down</u>	166.1	163.9	166.5	165.3	165.3	166.1	166.5
	CO		1931.2	1995.3	1962.4	1999.4	1991.6	2003.0	2029.9
	CO <sub>2</sub>		2.62	2.61	2.60	2.60	2.61	2.62	2.61
	NOx		146.3	139.3	146.1	156.2	147.3	146.0	149.9
XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX
BAG #3	HC	<u>Down</u>	166.3	163.7	166.6	165.0	165.2	166.2	165.1
	CO		1929.3	1988.7	1974.2	1999.6	1990.2	2004.8	2013.8
	CO <sub>2</sub>		2.62	2.61	2.60	2.60	2.61	2.62	2.59
	NOx		147.2	140.7	147.4	156.2	148.1	147.0	148.7
XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX
BAG #4	HC	<u>Down</u>	167.1	163.8	166.9	165.1	165.8	166.3	165.6
	CO		1946.6	1980.7	1982.8	2000.5	1998.7	2001.2	2021.6
	CO <sub>2</sub>		2.64	2.59	2.60	2.60	2.62	2.62	2.61
	NOx		148.4	142.4	147.9	156.7	148.9	147.3	149.7
XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX
BAG #5	HC	<u>Down</u>	165.0	165.4	166.8	164.8	165.9	165.4	164.0
	CO		1933.7	1992.3	1976.7	1996.6	1998.1	1991.2	1999.8
	CO <sub>2</sub>		2.61	2.61	2.61	2.60	2.61	2.60	2.58
	NOx		147.1	144.6	147.8	156.6	149.5	146.5	148.1
XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX
BAG #6	HC	<u>Down</u>	166.9	165.4	166.4	164.4	165.3	165.8	164.8
	CO		1942.7	1993.5	1968.6	1992.1	1995.7	1994.0	2010.6
	CO <sub>2</sub>		2.63	2.60	2.60	2.59	2.61	2.61	2.58
	NOx		140.2	144.7	147.8	156.0	149.0	147.0	149.2
XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX
DIR. FROM BLEND.,	HC	<u>Down</u>	168.3	167.0	167.4	165.0	166.9	166.5	166.1
	CO		1958.1	2002.8	1982.4	2000.0	2005.2	2004.8	2032.9
	CO <sub>2</sub>		2.65	2.62	2.61	2.59	2.62	2.63	2.61
	NOx		148.3	148.1	149.4	156.6	150.1	149.7	149.7

C.V.S. SAMPLING SYSTEM CORRELATION  
CRITICAL FLOW BLENDER

WEEK OF 9/25/77

		ROLLS 20	ROLLS 21	ROLLS 22	ROLLS 23	ROLLS 24	ROLLS 25	ROLLS 26	ROLLS 27
SPAN GAS CALIB.	HC	<i>DOWN</i>	<i>DOWN</i>	198.5	198.8	198.3	198.3	197.7	198.4
	CO			1412.2	1410.8	1483.4	1482.0	1481.1	1410.2
	CO <sub>2</sub>			3.04	3.04	3.04	3.03	3.04	3.03
	NOx			207.6	207.6	207.6	207.6	207.7	207.5
XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX
DIR. FROM BLEND.	HC	<i>DOWN</i>	<i>DOWN</i>	168.4	167.7	168.2	169.4	167.2	167.0
	CO			2025.6	1930.5	2018.2	2010.3	2000.0	2037.7
	CO <sub>2</sub>			2.64	2.61	2.67	2.63	2.62	2.62
	NOx			148.4	151.4	148.3	142.3	146.9	147.8
XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX
BAG #1	HC	<i>DOWN</i>	<i>DOWN</i>	164.8	167.4	167.8	168.6	166.8	167.1
	CO			1979.9	1927.5	2013.6	2025.8	1993.0	2022.7
	CO <sub>2</sub>			2.63	2.61	2.66	2.63	2.62	2.62
	NOx			138.6	148.8	146.3	143.8	142.7	147.3
XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX
BAG #2	HC	<i>DOWN</i>	<i>DOWN</i>	165.4	168.5	168.3	169.4	167.9	167.6
	CO			1989.4	1938.3	2015.9	2032.3	2008.9	2030.5
	CO <sub>2</sub>			2.64	2.63	2.67	2.63	2.65	2.62
	NOx			141.2	150.1	148.0	149.0	145.3	146.8
XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX
BAG #3	HC	<i>DOWN</i>	<i>DOWN</i>	165.4	168.5	168.0	168.1	168.1	166.9
	CO			1993.4	1938.4	2012.7	2025.5	2010.2	2026.2
	CO <sub>2</sub>			2.64	2.64	2.67	2.63	2.65	2.62
	NOx			142.2	150.6	148.3	146.2	146.3	148.6
XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX
BAG #4	HC	<i>DOWN</i>	<i>DOWN</i>	163.2	168.8	168.1	169.0	168.2	167.1
	CO			1959.7	1943.5	2012.8	2029.4	2010.2	2026.6
	CO <sub>2</sub>			2.60	2.64	2.67	2.64	2.65	2.62
	NOx			140.6	150.8	148.7	147.0	146.4	148.6
XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX
BAG #5	HC	<i>DOWN</i>	<i>DOWN</i>	165.2	168.6	168.2	169.7	167.7	162.9
	CO			1985.4	1942.3	2012.4	2036.1	2007.1	1968.8
	CO <sub>2</sub>			2.63	2.64	2.67	2.64	2.64	2.55
	NOx			142.2	150.7	148.8	148.3	146.1	145.2
XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX
BAG #6	HC	<i>DOWN</i>	<i>DOWN</i>	165.4	168.7	168.4	169.3	168.4	167.4
	CO			1994.0	1946.1	2011.0	2026.2	2014.5	2027.9
	CO <sub>2</sub>			2.64	2.64	2.67	2.64	2.66	2.62
	NOx			143.0	150.9	148.8	147.0	146.7	149.1
XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX	XXXXXXXXXXXXXX
DIR. FROM BLEND.	HC	<i>DOWN</i>	<i>DOWN</i>	167.9	168.2	170.3	170.8	169.2	166.4
	CO			2023.7	1947.2	2017.6	2037.4	2023.1	2034.4
	CO <sub>2</sub>			2.64	2.64	2.67	2.65	2.66	2.62
	NOx			148.8	150.7	148.7	149.5	148.2	150.7

HEATH INTERNATIONAL, INC. (RICHMOND INSTRUMENTS)

6-BAG CONSTANT VOLUME SAMPLER WITH REMOTE FILTER BOX

HEAT EXCHANGER, AIR INLET HEATED AND WATER COOLED

SUTORBILT BLOWER

4 SPEED LOUIS ALLIS PACEMAKER MOTOR

RANGE 3 PRIMARY RANGE USED , 380-400 CFM

40..

APPENDIX 3

F. Johnson C.H.E.

# BAG CROSS-CHECK

- 2 CONC. LEVELS
- CORR. FOR NO DECAY
- STATISTICAL SEARCH  
FOR OUTLIERS
- WEEKLY

# MIDRANGES

- ALL BAG RANGES
- $\pm 2\%$  LIMIT

# ZERO/SPAN

- PER BAG "GROUP"
- "PRE":  $\pm 0.2 \text{ mV}$
- "POST":  $\pm 1.0 \text{ mV}$

# NOX CONVERTER EFF.

- FED. REG. PROCEDURE
- DAILY
- LIMITS :
  - 98%
  - LEAK CHECKS

# LEAK CHECKS

- PROPANE INJECTION
- BAG CROSS CHECK
- BULK STREAM LEAK
- SAMPLE SYSTEM LEAK

# MONTHLY CHECKS

- H<sub>2</sub>O & CO<sub>2</sub> INT.
- BAG CURVES
- FID METHANE RESPONSE
- NDIR OPTIMIZATION

# OTHER CHECKS

- CO<sub>2</sub> BAG CONCENTRATIONS
- CVS REV'S, P<sub>in</sub>, ΔP
- ROLL REV'S
- DVU

# CVS SYSTEM

## Description

- Positive Displacement Pump
- Electronic Transducers - Pressure and Temperature
- Continuous Monitoring of CVS Parameters
- Computer Data Acquisition During Testing
- External Source of Dilution Air Supply

## Calibration

- Not on a 30-Day Schedule
- Calibration Verified by Propane Injection
- Propane Injections Performed Daily
- Flow Device - LFE
- LFE on the Outlet
- Plan to use SAO Technique
- Calibration Data Review and Validations

# CFO PROPANE INJ.

- DAILY
- $\pm 2\%$  AGREEMENT REQ'D
- ASSUME PURE PROPANE
- USE REAL GAS DENSITY

# ANALYZER CALibrations

## A. STANDARDIZE INSTRUMENTS, RANGES, AND CALIBRATION GASES

1. CELL LENGTH (%NL), FID FUEL

2. OVERLAPPING CALGASES

3. COMMON MANIFOLD FOR SPAN GASES

## B. MONITOR SECONDARY CURVE DEVIATIONS

TO DETECT DEGRADATION AND TO BETTER  
ESTIMATE VALUES

## C. RANGE - TO - RANGE CHECKS

1. SPAN, MIDSPAN, QTR. SPAN

# EPA ANALYZER RANGES

<u>HC</u>	<u>LCO</u>	<u>HCO</u>	<u>CO<sub>2</sub></u>	<u>NO<sub>x</sub></u>
250	1000	5000	5.0%	250
100	500	2500	2.5%	100
50	250		1.0%	50
	100			

APPENDIX 5

Dan PAULSELL - EPA

## SAC PROGRAM CAPABILITIES

- A. ASSESSES SITE/SITE, RANGE/RANGE CORRELATION AND REPEATABILITY
- B. DIAGNOSES INSTRUMENT PROBLEMS
  - 1. SPAN GAS VALVE LEAKS
  - 2. " " SET POINT ERROR
  - 3. CURVE SHIFT
  - 4. FID BURNER DETERIORATION
  - 5. CL CONVERTER EFF. LOSS
  - 6. SAMPLE SYSTEM INTEGRITY

APPENDIX 5

DON PAULSELL - EPA

# NO<sub>x</sub> CONVERTER EFFICIENCY

1. PERFORM ONCE PER WEEK
2. MINIMUM 90%, TYPICALLY 98+ %
3. MIXER IN EFFICIENCY CHECKER
4. 1% O<sub>2</sub>/AR FOR OZONE SOURCE

## CO<sub>2</sub> / H<sub>2</sub>O INTERFERENCE

1. HOPCALITE + ZERO AIR  $\Rightarrow$  CO IN N<sub>2</sub>
2. 3% CO<sub>2</sub> / N<sub>2</sub> BUBBLED THRU H<sub>2</sub>O <sup>ZERO GAS</sup>
3. < 3 ppm MAXIMUM, TYPICALLY .5 ppm

APPENDIX 5

Don Paulsell - EPA

# SAMPLE ANALYSIS CORRELATION

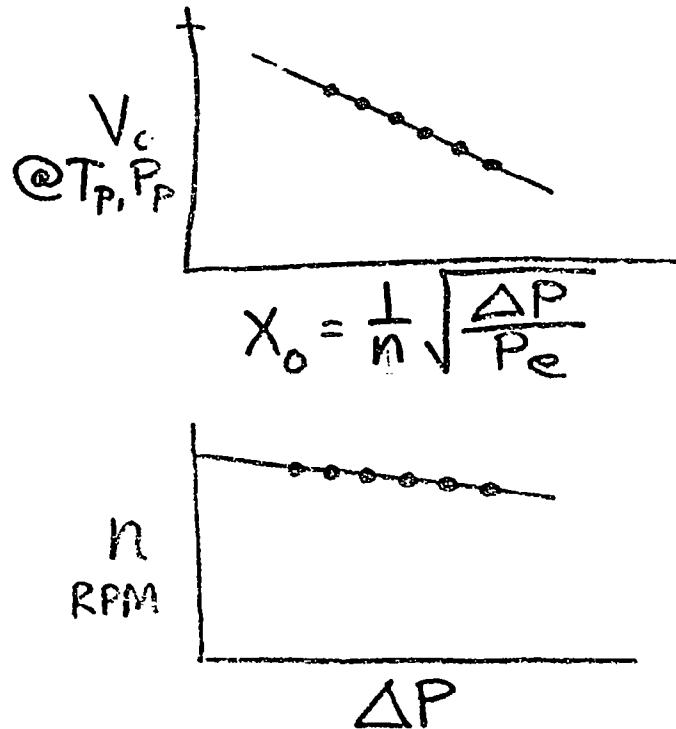
- A. ONE BAG/DAY - ALL LD ANALYZER SITES
- B. TWO WEEK ROTATION SCHEDULE
- C. CONTROL LIMITS HC CO CO<sub>2</sub> NO<sub>x</sub>  
±1 SIGMA 1.8% 1.6% .90% 1.9%
- D. CONTROL CHART FLAGS
  - 5 CONSECUTIVE +/-
  - 4/5 EXCEED 1 SIGMA
  - 2/3 EXCEED 2 SIGMA
  - TEST EXCEEDS 3 SIGMA

APPENDIX 5

DAN PAULSELL EPA

# CVS CALIBRATION

## A. PDP TYPE



$$V_o = m \cdot \left( \frac{1}{RPM_T} \sqrt{\frac{\Delta P}{P_e}} \right) + b$$

$$RPM_T = n \cdot \Delta P + a$$

$$RPM_A = \frac{REVS \cdot 60}{SECONDS}$$

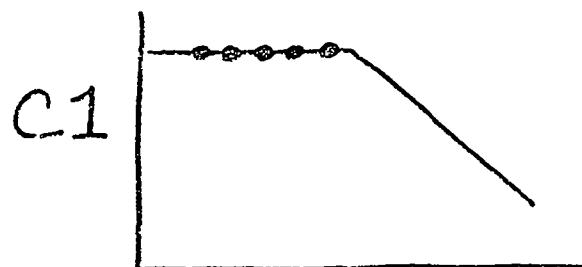
$$RPM_{RATIO} = \frac{RPM_A}{RPM_T} = 1.00 \pm .01$$

APPENDIX 5

DON PAWSELL - EPA

# CVS CALIBRATION

## B. CFV TYPE



$$\sigma_{C1} = \pm .3\% \quad P_{ABS}$$

$$Q_{THEO.} = 9.2853 D^2 \sqrt{T_{ABS}}$$

D = THROAT DIAM. (IN.)  
 $T_{ABS}$  = INLET ( $^{\circ}$ R)

$Q_{MEAS}$  = LFE FLOW @  
 CFV INLET COND.

$$Q_{RATIO} = \frac{Q_{MEAS}}{Q_{THEOR}} \Rightarrow \approx .985 - .990$$

TYPICAL

# TRACER GAS INJECTIONS

A. DENSITY VALUES FOR C<sub>3</sub>H<sub>8</sub> (<sup>INSTRUMENT</sup><sub>GRADE 99.5+</sub>)

1. PURE = 52.72 GMS/FT.<sup>3</sup>. (BEATTIE-BRIDGEMAN)

2. DILUTE = 51.88 " " (IDEAL GAS LAW)

B. CFO VS BOMB

- COMPARE ON MASS BASIS

- TO CONVERT  $Q_{Scfo} \Rightarrow M$ , USE 52.72 VALUE

- BOMB MASS IS DIRECT  $\Delta M \pm .002$  GMS.

C. TRACER GAS MANIFOLD

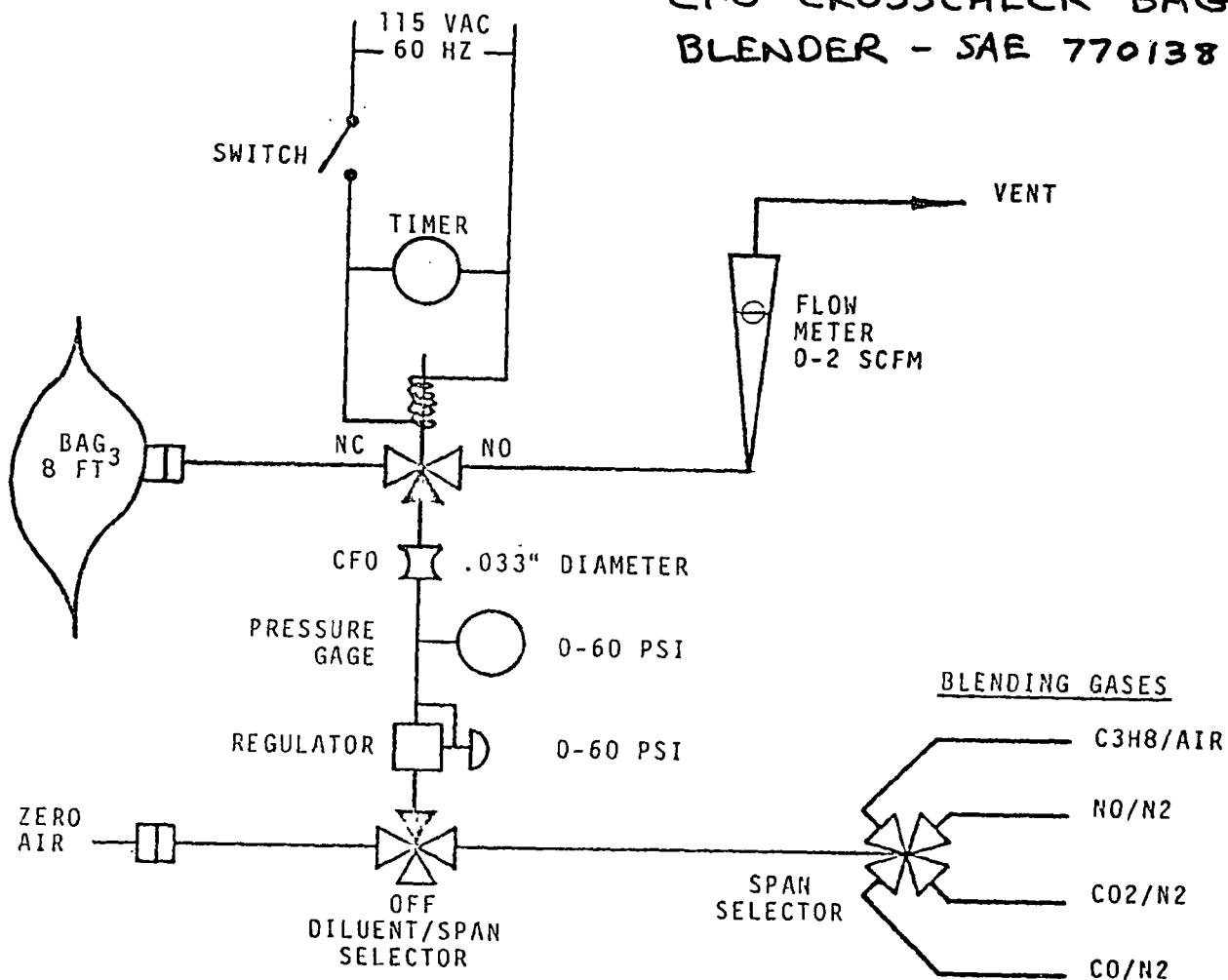
- CFO FABRICATION

- CFO CALIBRATION  $(Q = \frac{A \cdot P^2 + B \cdot P + C}{\sqrt{T}})$

APPENDIX 5

DO PAULSELL EPA

CFO CROSSCHECK BAG  
BLENDER - SAE 770138



5

APPENDIX 5

D. PAULSELL EPA

# Turner

821 Park Avenue  
Sycamore, Illinois 60178  
(815) 895-4545

November 16, 1976

U.S. Environmental Protection Agency  
2565 Plymouth Road  
Ann Arbor, Michigan 48105

Attention: Mr. Don Taulsell

Dear Mr. Taulsell:

Transmitted herewith are copies of Turner Company drawings S0-0001 and S0-0002 depicting our standard orifices and LP-3833, the filter used with those orifices. As we discussed yesterday, we buy the orifices from:

Starro Precision Products, Inc.  
37 North Union Avenue  
Elgin, Illinois 60120  
Tel: 312/741-3382

And the filters are made by:

Sintered Metals Inc.  
3390 Washington Avenue  
Boston, Massachusetts 02130

If further information is required or if I can be of assistance in any way please contact me.

Very truly yours,

  
George Barton, P.E.  
Manager, Operations Engineer

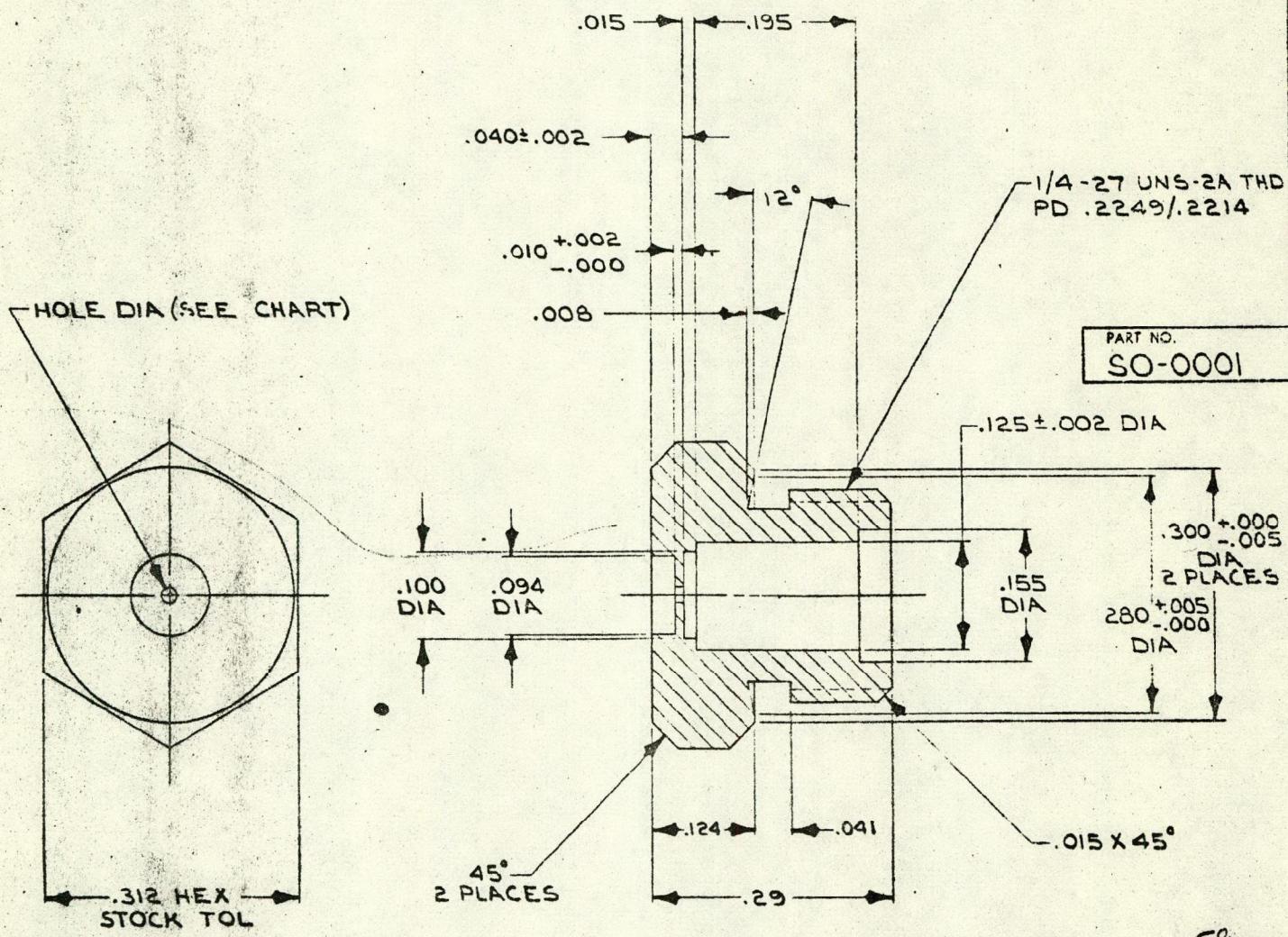
**NOTE: THE ORIFICE IN THIS  
PACKAGE WAS CALIBRATED  
FOR USE IN A PROPANE  
CFO MANIFOLD AT EPA.**

A Division of  
 Cleanweld Products, Inc.

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2.

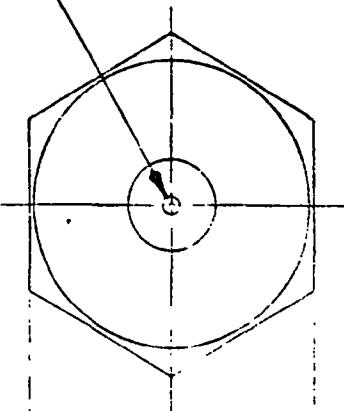
ART. NO.	DESCRIPTION NO.	HOLE DIA	IDENTIFICATION
P-4029-R	SO-0001-135	.0135 +.0005 -.0000	PLAIN - NICKEL FLASH BEFORE DRILLING



ART. NO.	SO-0001	ITEM NO.	5116	QTY.	1	UNIT	PC
DESCRIPTION	5/16 HEX FCY BRASS ROD	STOCK NO.	006 213 04	MANUFACTURER	TURNER CORPORATION	SHIP TO	SO-0001
SIZE	.312	FINISH	0.0	DO NOT SCALE DRAWINGS	STANDARD TO ERANCES		
WEIGHT	.000	TYPE	0.0	XX DFC. ± .015	XX DFC. ± .005		
STOCK NO.	006 213 04	APPROV'D BY	0.0	ANGLE ± 1°	ANGLE ± 1°		
DATE	0000	APPROV'D DATE	0000	SUPERVISOR	SUPERVISOR		
REMARKS	P/N 2-1714						

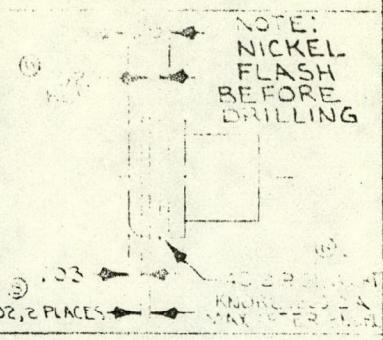
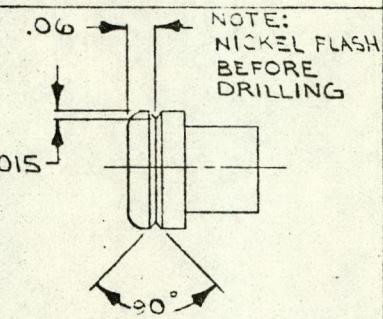
PART NO	DESCRIPTION NO.	HOLE DIA	IDENTIFICATION	PART NO	DESCRIPTION NO.	HOLE DIA
LP-3527-R	SO-0001-080	.0080 <sup>+.0000</sup> -.0005		LP-4079-R	SO-0001-135	.0135 <sup>+.0000</sup> -.0005
LP-3609-R	SO-0001-050	.0050 <sup>+.0005</sup> -.0000				
LP-3676-R	SO-0001-040	.0040 <sup>+.0005</sup> -.0000				
LP-3759-R	SO-0001-060	.0060 <sup>+.0005</sup> -.0000				

HOLE DIA (SEE CHART)



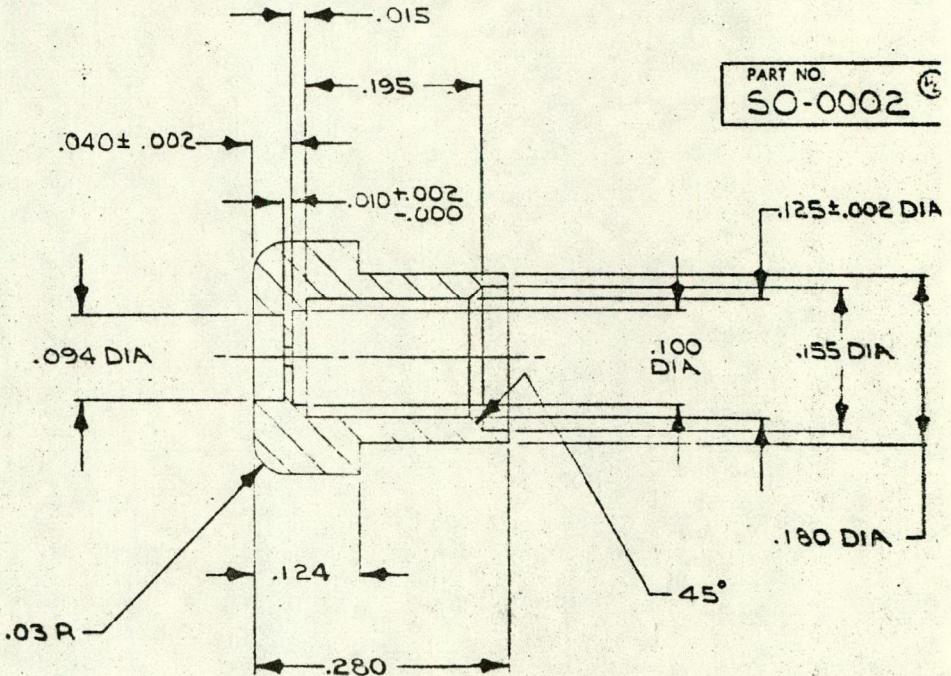
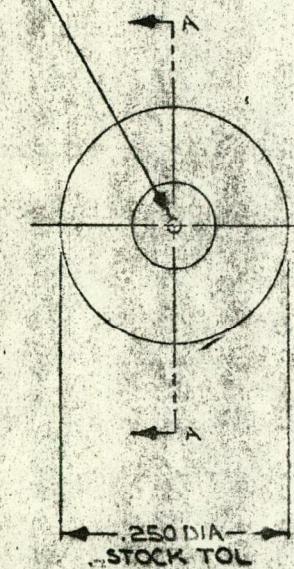
1/16 DI  
2 FIX STOCK TOL

4

PART NO.	DESCRIPTION	HOLE DIA. NO.	IDENTIFICATION
LP-4524-R	SO-0002-125	.125 +.0005 -.0000	 <p>NOTE: NICKEL FLASH BEFORE DRILLING</p>
LP-606-R	SO-0002-050	.0050 +.0000 -.0005	PLAIN
LP-3658-R	SO-0002-080	.0080 +.0000 -.0005	PLAIN - NI FLASH BEFORE DRILLING
④	SO-0002-180	.0180 +.0005 -.0000	 <p>NOTE: NICKEL FLASH BEFORE DRILLING</p>

← NOTE: THIS ORIFICE WAS USED FOR METERING C3H8 UNDER CRITICAL FLOW CONDITIONS. 70 PSIG ≈ 90 ppm FOR TYPICAL CVS.

—HOLE DIA (SEE CHART)

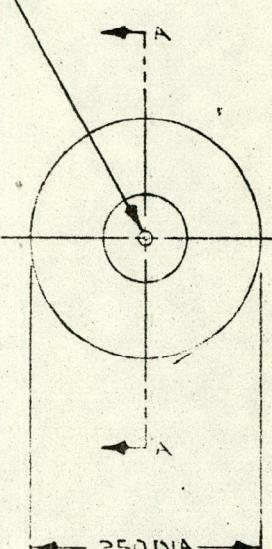


SECTION A-A

61

MAIL 1/4 DIA RND FCY BRASS ROD NO. 00611337	DRAWN BY C. H. TURNER	APR 1971	FOR USE ON SO-3052
RECORDED	APR 1971	TURNER CORPORATION	2000-05
APR 1971		APR 1971	

5.

ART #	DESCRIPTION	HOLE DIA. NO.	IDENTIFICATION	ART NO.	DESCRIPTION	HOLE DIA. NO.	
P-607-R	SO-0002-060	.0060 $^{+.0000}_{-.0005}$	(4)	.06 .015 90°	LP-4524-R	SO-0002-125	.0125 $^{+.0005}_{-.0000}$
P-3761-R	SO-0002-100	.0100 $^{+.0005}_{-.0000}$	(4)	.03 .06 40 D.P. STRAIGHT KNURL .260 DIA MAX AFTER KNURL NOTE: NICKEL FLASH BEFORE DRILLING	LP-606-R	SO-0002-050	.0050 $^{+.0000}_{-.0000}$
P-958-R	SO-0002-120	.0120 $^{+.0000}_{-.0005}$	(4)	.03 .06 40 D.P. STRAIGHT KNURL .260 DIA MAX AFTER KNURL	LP-3658-R	SO-0002-080	.0080 $^{+.0000}_{-.0000}$
P-3539-R	SO-0002-135	.0135 $^{+.0005}_{-.0000}$		.09 .02 REF .03 .02, 2 PLACES 40 D.P. STRAIGHT KNURL .260 DIA MAX AFTER KNURL, 2 PLACES	SO-0002-180		.0180 $^{+.0005}_{-.0000}$
P-2983-R	SO-0002-035	.0035 $\pm .0005$	(4)	.04 .09 .01 .012 GROOVES AS SHOWN NICKEL FLASH BEFORE DRILLING			HOLE DIA (SEE CHART)
SO-2902-055		.0055 $^{+.0000}_{-.0001}$	(4)				

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D. 0.23 ADDED TO .000 = .055

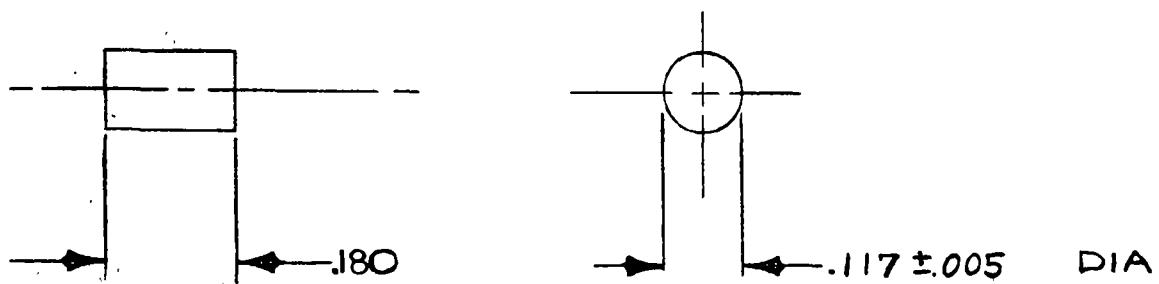
E. 0.23 ADDED SO-0002-180

F. EXCERANCED KNURL LINES

G. 0.23 ADDED

6.

PART NO.  
④ LP-3833



## Changes

B .62570 .180 WAS .310

A 3/10/70 .119 ± .003 WAS CHANGED TO .117 ± .005

7006/1 RELEASE

P-606-1	LP-607-1	LP-958-1	MATL BRONZE SINTERED POWDER (20 MICRON)	DO NOT SCALE DRAWINGS STANDARD TOLERANCES .XX DEC. ± .015 .XXX DEC. ± .005 ANGLE ± 1°	Part No W D U N T I D
LP-2333-1	LP-3539-1	LP-3658-1		SUPERCEDES E-519X	
LP-3761-1	LP-4044-1			SCALE 4 = 1	
			FINISH:		
			D.L	TURNER CORPORATION	
			DWG GLW 4261S	SYCAMORE, ILL	
			CHKD S/J	PART NAME	
NEXT ASSEM.	NEXT ASSEM.	NEXT ASSEM.	APPD	FILTER	

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# NBS TRACEABLE LFE CALIB.

CEESI

COLORADO  
ENGINEERING EXPERIMENT STATION  
INC.

OFFICE:  
P. O. Box 344  
Boulder, Colo. 80302  
Phone: 303-443-1344

LABORATORY:  
P. O. Box 41  
Nunn, Colo. 80648  
Phone: 303-397-2340

CALIBRATION OF A MERIAM LAMINAR FLOW ELEMENT  
MODEL: 50MC2-4SF SERIAL NUMBER: Y-72291R

FOR: U.S. ENVIRONMENTAL PROTECTION AGENCY

DATA FILE: EPA1A DATE: 10 DEC 1976

INLET DIA: 4 INCHES THROAT DIA: 4 INCHES

TEST GAS: AIR STD DENSITY= 0.074916 LBM/CU-FT

AT STANDARD CONDITIONS OF 529.69 DEG R AND 14.696 PSIA

DIFF: DIFFERENTIAL PRESSURE IN INCHES OF WATER AT 70 DEG F

ACFM: ACTUAL CUBIC FEET PER MINUTE

K FACTOR: ACFM\*VISCOSITY/DIFF

REY NO: INLET(PIPE) REYNOLDS NUMBER

SCFM: STANDARD CUBIC FEET PER MINUTE

PRESS: PRESSURE AT INLET TAP IN PSIA

TEMP: INLET TEMPERATURE IN DEGREES RANKINE

THIS # IS CALCULATED  
FROM CFV DATA (C<sub>i</sub>, P, T)

L	DIFF	ACFM	K FACTOR	REY NO	SCFM	PRESS	TEMP
1	1.215	66.71	5.5225 E-5	26791	67.80	14.693	521.13
2	1.809	99.29	5.5076 E-5	40073	101.20	14.698	519.77
3	2.392	130.38	5.4720 E-5	52612	132.90	14.703	519.91
4	2.975	161.70	5.4583 E-5	65151	164.65	14.696	520.23
5	3.587	194.70	5.4547 E-5	78366	198.15	14.699	520.59
6	4.188	226.13	5.4292 E-5	90860	229.90	14.696	521.04
7	4.816	259.23	5.4160 E-5	104080	263.49	14.703	521.40
8	5.406	290.88	5.4163 E-5	116624	295.40	14.700	521.76
9	6.019	322.67	5.3990 E-5	129238	327.48	14.699	522.03
10	6.658	356.30	5.3905 E-5	142592	361.42	14.696	522.21
11	7.274	388.26	5.3799 E-5	155250	393.71	14.702	522.57
12	7.621	406.01	5.3709 E-5	162263	411.61	14.703	522.75
13	7.627	436.08	5.3680 E-5	162216	411.52	14.698	522.80
14	7.285	388.30	5.3752 E-5	155038	393.38	14.698	522.93
15	5.433	291.04	5.4025 E-5	116178	294.82	14.699	523.02
16	2.990	161.79	5.4561 E-5	64604	163.92	14.699	522.93
17	1.209	66.37	5.5320 E-5	26568	67.36	14.708	522.39
18	0.640	35.37	5.5731 E-5	14148	35.87	14.703	522.48

AVERAGE VALUES FOR ABOVE RESULTS:

P = 14.7 PSIA DENSITY= 0.076074 LBM/CU-FT

T = 521.77 DEG R VISCOSITY= 1.0067E-6 LBM/INCH-SEC

Z = 0.99959 COMPRESSIBILITY FACTOR

$$^{\circ}K = 273.16 + ^{\circ}C$$

$$M_{STD} = 1.0185 \times 10^{-6} @ 70^{\circ}F$$

$$\left(\frac{lb_m}{in \cdot sec}\right) M = \left[ \frac{145.8 \times ^{\circ}K^{1.5}}{^{\circ}K + 110.4} \right] .0056 \times 10^{-7}$$

CEESI

COLORADO  
ENGINEERING EXPERIMENT STATION  
INC.

OFFICE:  
P. O. Box 344  
Boulder, Colo. 80302  
Phone: 303-443-1344

LABORATORY:  
P. O. Box 41  
Nunn, Colo. 80648  
Phone: 303-897-2340

MODEL: 50MC2-4SF      SERIAL NUMBER: Y-72291R  
DATA FILE: EPA1A      DATE: 10 DEC 1976

X POINTS EXCLUDED FROM AVERAGES. K(AVE)= 5.4402E-5 %DEV FROM K(AVE):  
L(0) R/1000 MTR READ L(0) -4 -3 -2 -1 0 +1 +2 +3 +4Z

08642086420864208642024680246802468024680

18	14.14	0.63951		.....	.....	.....	.....	0.....
17	26.56	1.209	1	.....	.....	.....	.....	0.....
2	40.07	1.8095		.....	.....	.....	.....	0.....
3	52.61	2.3919		.....	.....	.....	.....	0.....
16	64.6	2.9904	4	.....	.....	.....	00	.....
5	78.36	3.5869		.....	.....	.....	0	.....
6	90.86	4.1884		.....	.....	.....	0	.....
7	104.08	4.8159		.....	.....	.....	0	.....
15	116.17	5.4334	8	.....	.....	.....	00	.....
9	129.23	6.0188		.....	.....	.....	0	.....
10	142.59	6.6583		.....	.....	.....	0	.....
14	155.03	7.2849	11	.....	.....	.....	0	.....
13	162.21	7.6271	12	.....	.....	.....	00	.....

SCALE: ? 4

L0: 1.41 E+4	R 6.35 E+4	K= 5.52143 E-5	K/K(AVE)= 1.01493
STD DEV= 0.37 E-6		% STD DEV= 0.666	BASED ON 5 DATA PTS
MAX DEV= 0.52 E-6		% MAX DEV= 0.936	AT L=18 CHAUV= 1.6
MD: 6.35 E+4	R 1.13 E+5	K= 5.44286 E-5	K/K(AVE)= 1.00049
STD DEV= 0.19 E-6		% STD DEV= 0.351	BASED ON 5 DATA PTS
MAX DEV= -.27 E-6		% MAX DEV=-0.494	AT L= 7 CHAUV= 1.597
HI: 1.13 E+5	R 1.62 E+5	K= 5.38779 E-5	K/K(AVE)= 0.99036
STD DEV= 0.17 E-6		% STD DEV= 0.318	BASED ON 8 DATA PTS
MAX DEV= 0.29 E-6		% MAX DEV= 0.529	AT L= 8 CHAUV= 1.558

R(AVE)= 94591

K(AVE)= 5.4402E-5

R(L0)= 32038.      R(MD)= 80612.      R(HI)= 142420.

K = A + B\*R + C\*R\*R  
A= 5.5903E-5    B=-2.3589E-11    C= 6.5817E-17

X = X + Y\*(MTR READ) + Z\*(MTR READ)\* (MTR READ)  
X= 5.5887E-5    Y=-5.0786E-7    Z= 3.0976E-8  
BASED ON ABOVE TEST DATA (P,T,GAS)  
AND ASSUMING K CORRELATES WITH MTR READ

THIS CALIBRATION IS TRACEABLE TO NBS.  
THE FLOW MEASUREMENT ACCURACY IS ESTIMATED TO BE:  $\pm 0.5\%$  W.S.I.D.  
COLO ENGINEERING EXPERIMENT STATION INC, BX 41, NUNN CO 80648

CALIBRATION DATA FOR LFE # Y-72291R  
12/10/76

DATA POINT	<sup>2</sup> SCFM	<sup>3</sup> PABS	<sup>4</sup> TABS	<sup>5</sup> ACFM	<sup>6</sup> VISCOSITY $\mu \times 10^6$	<sup>7</sup> K <sub>105</sub> $(^\circ H_2O)$	<sup>8</sup> $\Delta P$ $(^\circ H_2O)$	<sup>9</sup> CFM <sup>5</sup>	R #
1	67.80	14.693	521.13	66.71	1.0057	5.5025	1.015	65.8736	26791
2	101.20	14.698	519.77	99.29	1.0037	5.5076	1.809	97.8464	40073
3	132.90	14.703	519.91	130.33	1.0034	5.4720	2.392	108.5113	52612
4	164.65	14.696	520.23	161.70	1.0044	5.4583	2.975	159.4555	65151
5	198.15	14.699	520.59	194.70	1.0049	5.4547	3.587	192.1043	78366
6	229.90	14.696	521.04	226.13	1.0056	5.4292	4.188	223.2643	40860
7	263.49	14.703	521.40	259.23	1.0061	5.4160	4.816	256.0846	104080
8	295.40	14.700	521.76	290.88	1.0067	5.4163	5.406	287.5023	116624
9	327.48	14.699	522.03	322.67	1.0071	5.3790	6.019	319.0512	12838
10	361.42	14.696	522.31	356.30	1.0074	5.3705	6.653	352.3932	140592
11	393.71	14.702	522.57	388.26	1.0079	5.3799	7.274	384.2135	155250
12	411.61	14.703	522.75	406.01	1.0082	5.3709	7.621	401.8554	162263
13	411.52	14.693	522.80	406.08	1.0082	5.3680	7.627	401.9850	162216
14	393.38	14.698	522.93	388.30	1.0084	5.3752	7.285	384.4584	155038
15	294.82	14.699	523.02	291.04	1.0086	5.4025	5.433	253.1991	116178
16	163.92	14.699	522.93	161.79	1.0084	5.4561	2.990	160.1813	64604
17	67.36	14.703	522.39	66.37	1.0076	5.5300	1.209	65.6607	26568
18	35.87	14.703	522.48	35.37	1.0078	5.5731	0.640	34.9467	14148

DATA REDUCTION OF CEESI SUPPLIED DATA  
TO GET INPUT FOR  $[CFM = A \cdot \Delta P + B \cdot \Delta P^2]$

$$^1 @ 539.69 ^\circ R \quad 14.696 \text{ PSI}$$

$$^2 ACFM = SCFM \cdot \frac{14.696}{PABS} \cdot TABS$$

$$^3 \gamma = \left[ \frac{145.8 \times K^{1.5}}{K + 110.4} \right] \times \frac{529.69}{.0056 \times 10^{-7}}$$

$$^4 K = ACFM \cdot \frac{\gamma}{\Delta P}$$

$$^5 CFM = ACFM \cdot \frac{\gamma}{1/STD(700)}$$

$$\gamma_{TD} = 1.0185 \times 10^{-6}$$

\*\*\*\* PROCESSED: 13:05:40 07-11-77

\*\*\*\*\*  
\*\*\* ANALYZER CALIBRATION CURVE ANALYSIS \*\*\*  
\*\*\*\*\*

END CALIB AT TIME :	0: 0	ANALYZER VENDOR :	SAMPLE FLOW RATE :	0.0	VALID DEFL. UPPER LIMIT :	110.000
CALIBRATION DATE :	0-0-0	INSTRUMENT NAME :	MONITOR SET POINT :	0.0	VALID DEFL. LOWER LIMIT :	-10.000
TEST SITE NUMBER :		FID DECAL ID NO :	ZERO GAIN SETTING :	0.0	RANGE CHANGE UPPER LIMIT :	100.000
GAS ANALYZED :	PROPANE	SIGNAL LEAD :	SPK GAIN SETTING :	0.0	RANGE CHANGE LOWER LIMIT :	20.000
DILUTENT GAS :	OZONE	HARDWARE RANGE :	THIN READING :	0.0	FULL-SCALE (100%) DEFL. :	100.000
CONCENTRATION UNIT:	PPM	USAGE :	FID AIR PRESSURE :	0.0	FULL-SCALE (100%) VOLTAGE:	0.0
STANDARD FAR RANGE:	18	CALIB G/S SOURCE :	FID FUEL PRESSURE :	0.0	FULL-SCALE (100%) CONC. :	522.9
OPERATOR ID NO :	22087	CALENDAR DECAL ID :	FID SAMP PRESSURE :	0.0	RECORDER TYPE :	

FILE COMMENT : NOTE: X AXIS IS IN P#10 C  
 OPERATOR COMMENT : CFM VS P FID LEE # Y-772910 : 12/10/76

CYLINDER NUMBER	THREE-DIGIT ALLOY ID	CONCENTRATIONS		ANALYZED SIGNAL MEASURED CORRECTED	CALIBRATION DATA X M C	CURVE FIT DEVIATIONS		
		LEAD	DILUENT	(ALLOY/ED)	CALCULATED	% POINT	% FULL-SCALE	% FROM LAST CALIBRATION
	X			0.0				
	X			0.0				
0.0	0.0	0.0		65.37	65.44	12.150	12.150	
0.0	0.0	0.0		97.35	97.39	18.090	18.099	
0.0	0.0	0.0		124.51	124.49	23.420	23.420	
0.0	0.0	0.0		154.46	154.33	29.750	29.750	
0.0	0.0	0.0		192.10	191.17	35.870	35.870	
0.0	0.0	0.0		223.26	223.44	41.880	41.880	
0.0	0.0	0.0		255.08	255.34	48.160	48.160	
0.0	0.0	0.0		287.50	287.22	54.060	54.060	
0.0	0.0	0.0		319.05	319.11	60.190	60.190	
0.0	0.0	0.0		352.40	352.22	66.580	66.580	
0.0	0.0	0.0		384.21	383.48	72.740	72.740	
0.0	0.0	0.0		401.99	401.32	76.210	76.210	
0.0	0.0	0.0		401.99	402.33	76.270	76.270	
0.0	0.0	0.0		384.46	384.55	72.450	72.450	
0.0	0.0	0.0		288.20	288.63	54.330	54.330	
0.0	0.0	0.0		160.19	160.18	29.900	29.900	
0.0	0.0	0.0		65.66	65.16	12.090	12.090	
0.0	0.0	0.0		35.00	34.56	5.400	5.400	
NONLINEARITY = -0.4 PERCENT				AVERAGE DEVIATION		0.069	0.034	0.0

\*\*\*\*\* PROCESSED: 13:05:40 07-11-77

```
***** ANALYZER CALIBRATION CURVE ANALYSIS *****
```

END CALIB AT TIME : 0:0 ANALYZER VERSION : ZERO SPAN TYPE : 1  
 CALIBRATION DATE : 0-0-0 INSTRUMENT NAME : CURVE FORM : 1  
 TEST SITE NUMBER : EPA DECAL ID NO : DEGREE FIT : 2  
 GAS ANALYZED : PROpane SIGNAL LEAD : WEIGHTING FACTOR : 1  
 FULL-SCALE CONC : 522.4 HARDWARE RANGE :  
 CONCENTRATION UNIT: ppm USAGE :  
 STANDARD LAB RANGE: 18 OPERATOR ID NO : 22087

## EQUATIONS AND COEFFICIENTS

$x = x$  ;  
 $c$   
 $R() = 0.6$

$\frac{4}{C} \cdot A_5 * x^4 + \frac{3}{C} \cdot A_4 * x^3 + \frac{2}{C} \cdot A_3 * x^2 + A_2 * x + A_1 = \text{PPM PROPANE/OZONE}$

$A_1 = 0.0$   
 $A_2 = 0.5411711E+01$   
 $A_3 = -0.1826475E-02$   
 $A_4 = 0.0$   
 $A_5 = 0.0$

CALIBRATION TABLE - PERCENT FULL SCALE DEFLECTION VS. RPM PROPANE/ZOZONE

## QUALITY CONTROL COMMENTS

\*\*\*\*\* CURVE NOT STORED ON FILE

COLORADO ENGINEERING EXPERIMENT STATION, INC.

P. O. Box 344  
Boulder, Colorado 80302

Date: December 15, 1976

This is to certify that the instrumentation used in the  
calibration of Meriam Laminar Flow Element  
Model No. 50MC2-4SF Serial No. Y-72291R  
is traceable to the National Bureau of Standards.

Walter F. Seidl

President ( Acting )

**CEESI**

**COLORADO  
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Boulder, Colo. 80302  
Phone: 303-443-1344

**LABORATORY:**  
P. O. Box 41  
Nucla, Colo. 80648  
Phone: 303-897-2340

Date: December 15, 1976

This is to certify that the accuracy of the calibration  
 on Meriam Laminar Flow Element  
 Model No. 50MC2-4SF Serial No. Y-72291R  
 is Within plus or minus 0.4 percent of reading.

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---

Walter F. Seidl

President ( Acting )

70

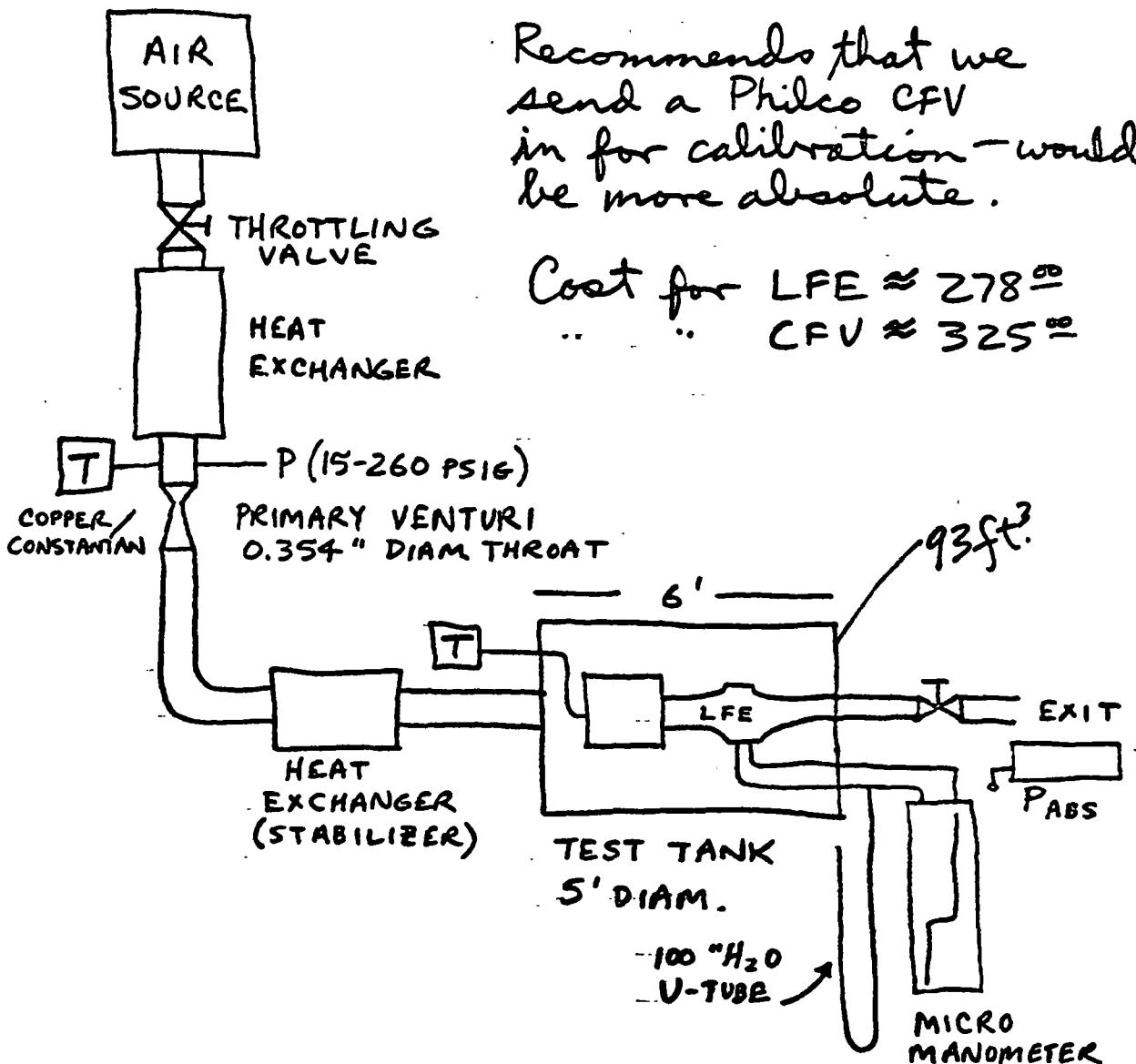
WALT SEIDL  
303-534-7535

327-0111

STEVE CALDWELL  
LAB. TECHNICIAN  
FTS 8-327-0111

CEESI  
303-897-2340

### TEST SETUP FOR LFE CALIB.



**CEESI**

**COLORADO  
ENGINEERING EXPERIMENT STATION  
INC.**

**OFFICE:**  
P. O. Box 344  
Boulder, Colo. 80302  
Phone: 303-443-1344

February 7, 1974

**LABORATORY:**  
P. O. Box 41  
Nunn, Colo. 80648  
Phone: 303-897-2340

MEMO:

To our customers

Re: Shipping Methods, in order of preference

1. United Parcel Service (where available)
 

Address: Colorado Engineering Experiment Station  
Missile Site  
Nunn, Colorado  
Limitations: 100 lb. per day  
Insurance: \$5,000.00 max.  
Receipt is provided
2. U. S. Postal Service (parcel post)
 

Address: Colorado Engineering Experiment Station  
P. O. Box 41  
Nunn, Colorado 80648  
Limitations: 70 lb.  
Length & Girth = 100" max.  
Insurance: \$200.00 max.  
Receipt is provided if insured. If not insured, a Certificate of Mailing costs 5 cents.
3. Bus Package Express
 

Address: Colorado Engineering Experiment Station  
Fort Collins, Colorado  
On arrival phone: 484-9365  
Limitations: 100 lb. / package  
5 packages / shipment  
Length & Width & Height = 141" max.  
Height = 60" max.  
Insurance: \$250.00 max.  
Receipt is provided.

MEMO: To our customers  
February 7, 1974  
Page 2

3. Motor Freight (TUR)

Address: Colorado Engineering Experiment Station  
Missile Site  
Nunn, Colorado

Limitations: Check that they are not on strike at  
Denver. (Alternate truck line from  
Denver to our site: Miller Bros., Inc.)

5. Air Freight

To Denver: Motor freight to our site (see above)

To Cheyenne: We can arrange pick up.

Limitations to Cheyenne:

Frontier - Weight - 200 lb.

Width 23", Length 40", Height 43"

Western - Weight 250 lb.

500 lb with special arrangements.

Max.	Width	Height	Length
	12"	10"	186"
	24"	25"	157"
	34"	20"	124"
	30"	45"	86"

Insurance: No limit

Receipt is provided

3. REA Express

Address: Colorado Engineering Experiment Station  
Loveland, Colorado

On arrival, phone: 397-2340

or: 434-9365

Limitations: None

Insurance: No limit

ENGINEERING EXPERIMENT STATION  
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LIBRATION OF A MERIAM LAMINAR FLOW ELEMENT  
 M. DEL: 50MC2-8F S/N: F62502TR EPA TAG: 092015  
 F. R: U.S. ENVIRONMENTAL PROTECTION AGENCY ORDER: CD-7-20876-A  
 D. TA FILE: EPAS DATE: 18 AUGUST 1977  
 I. INLET DIA: 6 INCHES THROAT DIA: 12 INCHES  
 S. STD GAS: AIR STD DENSITY= 0.074916 LBM/CU-FT  
 AT STANDARD CONDITIONS OF 529.69 DEG R, AND 14.696 PSIA  
 C. DP: DIFFERENTIAL PRESSURE IN INCHES OF WATER AT 68 DEG F  
 F. ACM: ACTUAL CUBIC FEET PER MINUTE  
 K. FACTOR: ACM\*VISCOSITY/DIFF.  
 REYN: INLET(PIPE) REYNOLDS NUMBER  
 SCFM: STANDARD CUBIC FEET PER MINUTE  
 PRESS: PRESSURE AT INLET TAP IN PSIA  
 T. IP: INLET TEMPERATURE IN DEGREES RANKINE

	DIFF	ACFM	K FACTOR	REY NO	SCFM	PRESS	TEMP
1	7.625	2017.63	2.7072 E-4	519658	2006.61	14.701	532.79
2	7.814	2064.82	2.6961 E-4	535063	2060.40	14.698	530.89
3	7.633	2019.37	2.7059 E-4	520135	2007.87	14.692	532.59
4	7.444	1973.03	2.7107 E-4	508556	1962.88	14.698	532.49
5	6.958	1849.40	2.7148 E-4	477947	1842.33	14.692	531.59
6	6.209	1655.89	2.7277 E-4	426565	1646.66	14.694	532.59
7	5.399	1443.24	2.7336 E-4	372000	1435.82	14.698	532.49
8	6.179	1649.66	2.7231 E-4	427611	1646.15	14.692	530.69
9	4.573	1231.25	2.7520 E-4	317599	1225.31	14.694	532.19
10	3.814	1029.03	2.7608 E-4	264819	1022.72	14.694	532.89
11	3.046	825.56	2.7729 E-4	212598	820.81	14.694	532.69
12	3.800	1027.02	2.7639 E-4	264652	1021.48	14.694	532.49
13	2.274	616.41	2.7724 E-4	158716	612.78	14.692	532.69
14	1.512	409.31	2.7704 E-4	105334	406.79	14.694	532.89
15	1.374	372.54	2.7756 E-4	95690	369.82	14.691	533.39
16	1.148	312.93	2.7863 E-4	80667	311.31	14.694	532.39
17	0.933	254.29	2.7852 E-4	65624	253.15	14.696	532.09
18	0.719	196.08	2.7856 E-4	50600	195.16	14.691	531.99
19	0.934	254.24	2.7820 E-4	65637	253.12	14.692	531.89

AVERAGE VALUES FOR ABOVE RESULTS:

P= 14.694 PSIA DENSITY= 0.07454 LBM/CU-FT  
 T= 532.3 DEG R VISCOSITY= 1.0224E-6 LBM/INCH-SEC  
 Z: 0.99965 COMPRESSIBILITY FACTOR

10

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Boulder, Colo. 80302  
Phone: 303-443-1344

LABORATORY:  
P.O. Box 41  
Nunn, Colo. 80648  
Phone: 303-597-2340

MODEL: 50MC2-8F S/N: F62502TR EPA TAG: 092015  
DATA FILE: EPAS DATE: 18 AUGUST 1977

Y POINTS EXCLUDED FROM AVERAGES. K(AVE)= 2.7488E-4 ZDEV FROM K(AVE)  
(0) R/1000 MTR READ L(0) -4 -3 -2 -1 0 +1 +2 +3 +4%  
08642086420864208642024680246802468024680

18	50.59	0.71933	.....	0	.....
17	65.62	0.93317	19	.....	00.....
16	80.66	1.1484	.....	0	.....
15	95.68	1.3744	.....	0	.....
14	105.33	1.5118	.....	0	.....
13	158.71	2.2744	.....	0	.....
11	212.59	3.0456	.....	0	.....
12	264.65	3.8	10	.....	90.....
9	317.59	4.5734	.....	0	.....
7	372	5.3993	.....	0	.....
6	426.56	6.2091	8	.....	90.....
5	477.94	6.9575	.....	0	.....
4	508.55	7.4436	1	.....	90.....
3	520.13	7.633	2	.....	0,0.....

SCALE, ? 4

L: 5.06 E+4	R 2.12 E+5	K= 2.77965 E-4	K/K(AVE)= 1.01124
S'D DEV= 0.67 E-6	Z STD DEV= 0.242	BASED ON 7 DATA PTS	
Y'X DEV= -.93 E-6	Z MAX DEV=-0.334	AT L=14	CHAUVE= 2.35
Z'D DEV= 2.12 E+5	K= 2.75666 E-4	K/K(AVE)= 1.00287	
S'D DEV= 0.15 E-5	Z STD DEV= 0.540	BASED ON 5 DATA PTS	
Y'X DEV= -.23 E-5	Z MAX DEV=-0.836	AT L= 7	CHAUVE= 1.222
Z': 3.74 E+5	R 5.35 E+5	K= 2.71224 E-4	K/K(AVE)= 0.98671
S'D DEV= 0.11 E-5	Z STD DEV= 0.396	BASED ON 7 DATA PTS	
Y'X DEV= -.16 E-5	Z MAX DEV=-0.594	AT L= 2	CHAUVE= 1.882

R AVE)= 287866

K(AVE)= 2.7488E-4

R(L0)= 88895. R(MD)= 286330. R(HI)= 487930.

$$Y = A + B*R + C*R*R$$

$$A = 2.7834E-4 \quad B = -1.87E-12 \quad C = -2.6043E-17$$

$$K = X + Y*(MTR READ) + Z*(MTR READ)*(MTR READ)$$

$$X = 2.7838E-4 \quad Y = -1.8012E-7 \quad Z = -1.1576E-7$$

BASED ON ABOVE TEST DATA (P,T,GAS)

AND ASSUMING K CORRELATES WITH MTR READ

THIS CALIBRATION IS TRACEABLE TO NBS.

THE FLOW MEASUREMENT ACCURACY IS ESTIMATED TO BE:  $\pm 0.5\%$  U.S.G.P.

COLORADO ENGINEERING EXPERIMENT STATION INC., BX 41, NUNN CO 80648

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DATA? EPASOUT  
NUMBER OF POINTS? 19

MEAN VALUE OF X = 287868.  
MEAN VALUE OF Y = 2.74875E-4  
STD ERROR OF Y = 3.17808E-6

POLYFIT OF DEGREE 2 INDEX OF DETERM = 0.983963      WHAT NEXT? 2

TERM COEFFICIENT

2.78637E-4  
-4.29867E-12  
-2.21441E-17

X ACTUAL	Y-ACTUAL	Y-CALC	DIFF	PCT-DIFF
-19658	2.70722E-4	2.70424E-4	2.98425E-7	0.11
-135060	2.6961E-4	2.69998E-4	-3.87643E-7	-0.144
-520140	2.7059E-4	2.7041E-4	1.79595E-7	0.066
-508560	2.7107E-4	2.70724E-4	3.46026E-7	0.128
-477950	2.7148E-4	2.71524E-4	-4.42407E-8	-0.016
-426570	2.7277E-4	2.72774E-4	-4.23702E-9	-0.002
-312000	2.7336E-4	2.73974E-4	-6.13808E-7	-0.224
-27610	2.7231E-4	2.7275E-4	-4.40094E-7	-0.161
-317600	2.752E-4	2.75038E-4	1.61621E-7	0.059
-264820	2.7608E-4	2.75946E-4	1.34028E-7	0.049
-22600	2.7729E-4	2.76723E-4	5.67479E-7	0.205
-264650	2.7639E-4	2.75949E-4	4.41304E-7	0.16
-198720	2.7724E-4	2.77397E-4	-1.57166E-7	-0.057
-105330	2.7704E-4	2.77939E-4	-8.98853E-7	-0.323
-95690	2.7756E-4	2.78023E-4	-4.63202E-7	-0.167
-80667	2.7863E-4	2.78146E-4	4.83548E-7	0.174
-61624	2.7852E-4	2.7826E-4	2.60155E-7	0.093
-50600	2.7856E-4	2.78363E-4	1.96902E-7	0.071
-40637	2.782E-4	2.7826E-4	-5.97522E-8	-0.021

STD ERROR OF ESTIMATE FOR Y = 0.00153207

COLORADO  
ENGINEERING EXPERIMENT STATION  
INC.

LAMINAR ELEMENT FLOW TABLE

MODEL: 50MC2-BF S/N: F62502TR EPA TAG: 092015

FOR: U.S. ENVIRONMENTAL PROTECTION AGENCY ORDER: CD-7-20876-A

CALIBRATION DATA FILE: EPAS DATE: 18 AUGUST 1977

K FACTORS BASED ON LEAST-SQUARES FIT TO CALIBRATION DATA

FLOWRATES CORRECTED TO 14.696 PSIA AND 70 DEGREES FAHRENHEIT

DIFF: DIFFERENTIAL PRESSURE IN INCHES OF WATER AT 68 DEG F

ACFM: FLOWRATE IN ACTUAL CUBIC FEET PER MINUTE

K FACTOR: ACFM\*VISCOSITY/DIFF

REY NO: INLET (PIPE) REYNOLDS NUMBER

SCFM: FLOWRATE IN STANDARD CUBIC FEET PER MINUTE

STANDARD CONDITIONS: 14.696 PSIA AND 70 DEGREES FAHRENHEIT

DIFF	ACFM	K FACTOR	REY NO	SCFM
0.750	204.96	2.7834 E-4	53320	204.96
1.000	273.16	2.7822 E-4	71061	273.16
1.250	341.28	2.7808 E-4	88781	341.28
1.500	409.32	2.7793 E-4	106479	409.31
1.750	477.25	2.7776 E-4	124151	477.24
2.000	545.07	2.7758 E-4	141795	545.07
2.250	612.78	2.7739 E-4	159408	612.78
2.500	680.36	2.7718 E-4	176988	680.35
2.750	747.80	2.7696 E-4	194533	747.80
3.000	815.10	2.7673 E-4	212039	815.09
3.250	882.24	2.7648 E-4	229504	882.23
3.500	949.22	2.7623 E-4	246926	949.21
3.750	1016.02	2.7595 E-4	264303	1016.01
4.000	1082.64	2.7567 E-4	281633	1082.63
4.250	1149.07	2.7537 E-4	298912	1149.05
4.500	1215.29	2.7506 E-4	316140	1215.28
4.750	1281.31	2.7474 E-4	333313	1281.30
5.000	1347.12	2.7441 E-4	350429	1347.10
5.250	1412.70	2.7407 E-4	367487	1412.68
5.500	1478.05	2.7371 E-4	384500	1478.03
5.750	1543.15	2.7334 E-4	401437	1543.14
6.000	1608.02	2.7296 E-4	418311	1608.00
6.250	1672.62	2.7257 E-4	435118	1672.61
6.500	1736.97	2.7217 E-4	451858	1736.95
6.750	1801.05	2.7176 E-4	468528	1801.03
7.000	1864.86	2.7134 E-4	485127	1864.84
7.250	1928.38	2.7091 E-4	501653	1928.36
7.500	1991.62	2.7047 E-4	518104	1991.60
7.750	2054.57	2.7001 E-4	534480	2054.55
8.000	2117.22	2.6955 E-4	550778	2117.20

DYNAMOMETER SYSTEM

<u>QC CHECK</u>	<u>TECHNIQUE</u>	<u>FREQUENCY</u>	<u>ACCURACY</u>
1. Driving Aid Calibration	Roll Revolution Count	30 Days	$\pm 0.1$ mph
2. Tachometer Calibration	Digital Counter	BiMonthly	$\pm 10$ rpm
3. Driving Aid Check	Roll Revolution Count	Daily	$\pm 0.1\%$
4. Frictional HP-Road Load HP Check	Coastdown	Weekly	$\pm 0.5$ HP

APPENDIX 6a

BRUCE GARDNER, FORD

QUICK COASTDOWNS

AFTER COMPLETE DYNAMOMETER CALIBRATION AND COASTDOWNS

<u>DATE</u>	<u>IND HP @ 50</u>	<u>TIME</u>	<u>ABSORBED HP</u>
2-9-75	9.8 HP	13.8 sec	19.80 HP
		13.8	19.80
		13.8	19.80
2-10-75	9.8	13.4	20.39
		13.6	20.09
		13.8	19.80
		14.0	19.52
		14.0	19.52
		14.0	19.52
2-11-75	9.9	13.6	20.09
		13.6	20.09
		13.8	19.80
		13.8	19.80
		13.8	19.80
2-12-75	9.8	13.6	20.09
		13.8	19.80
		13.8	19.80
		13.8	19.80
2-13-76	9.8	13.6	20.09
		13.8	19.80
		13.8	19.80
		13.8	19.80

QUICK COASTDOWNS  
 CAR #258 ROLLS #27

COASTDOWN WITH VEHICLE ON ROLLS AFTER TEN MINUTE WARM-UP  
 4500 LB., AUTO ROAD LOAD

<u>DATE</u>	<u>IND HP @ 50</u>	<u>TIME</u>	<u>ABSORBED HP</u>
2-2-75	9.8	13.8	19.80
		13.8	19.80
		13.8	19.80
		14.0	19.52
		14.0	19.52
		14.0	19.52
2-3-75	9.8	13.8	19.80
		13.8	19.80
		14.0	19.52
		14.0	19.52
		14.0	19.52
		13.6	20.09
2-4-75	9.8	13.8	19.80
		13.8	19.80
		13.8	19.80
		13.8	19.80
2-5-75	9.9	13.2	20.70
		13.4	20.39
		13.4	20.39
		13.6	20.09
		13.8	19.80
		13.6	20.09
		13.8	19.80
		13.8	19.80
2-6-75	10.0	13.8	19.80
		13.8	19.80
		13.8	19.80
		13.8	19.80

# DYNAMOMETER SYSTEM

## General

- Operate in the Automatic Mode
- Speed and Horsepower Calibration per Federal Register
- Individual Interia Weight Setting Calibrations
- Computerized Least Squares Curve Fit
- Computer Program Generates Actual vs Indicated H.P.
- Thumbwheel Switches for Setting H.P.
- Dynamometer Uniformity
  - Roll Spacing - 17.25 inches
  - Machined Rolls
  - Laser Beam Alignment
  - Solid Bearing Supports
  - Uniform Circumference

## Calibration

- Driver's Aid Linearity Checks
- Full Dynamometer Speed and Horsepower Verification - 30 Day
- [REDACTED] H.P. Checks Before Test
- Dynamometer Verification Unit
- 160 Pulse/rev. Optical Encoder
- Computer Data Acquisition During Testing
- Back-up Display Devices
- Live-Synchronized Stroboscope Speed Calibration
- Dynamometer Coastdown Vehicle

T.L.S - 10/5/77  
G.M. P.G.

# "DVU" MONITORING

EPA IV-1

- A. IW ENGAGEMENT - MICROSWITCH DECODER/ALARM
- B. SPEED (RR) AND TORQUE
- C. HP READOUT @ 50 MPH (FR)
  - MAGNETIC P/U ON TACH DRIVE GEAR (24 TEETH) IS USED TO TRIGGER Hp.
- D. TWO ROLL REV COUNTERS

EPA IV - 2

N= 812	ROLL REVS		DATA		
	$\bar{x}$	SIGMA	95% CL.	MILES	%Δ
BAG 1	8407.	77.7	1.8%	3.6058	.4
BAG 2	9116.	105.5	2.3%	3.9010	1.1
BAG 3	8409.	78.6	1.9%	3.6067	.4
HWFE	24004.	187.2	1.6%	10.295	.5
N= 691					

QC FLAG = AVERAGE RR  $\pm 2\%$

REAR ROLL ENCODER = 320 P/R

(160 P/R DRIVEN @ 2:1 ROLL SPEED)

DVU DIVIDES BY 32 TO COUNT 10 P/R

VEHICLE CROSS CHECK LIMITS

EMISSION LEVEL GRAMS/MILE	<u>HC</u> 1.40	<u>CO</u> 8.5	<u>NO<sub>x</sub></u> 3.3	<u>CO<sub>2</sub></u> 600
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MAXIMUM PERCENT VARIATION	5.0%	10.0%	8.0%	3.0%
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EMISSION LEVEL GRAMS/MILE	<u>HC</u> 0.5	<u>CO</u> 4.0	<u>NO<sub>x</sub></u> 2.3	<u>CO<sub>2</sub></u> 670
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MAXIMUM PERCENT VARIATION	10.0%	15.0%	10.0%	3.0%
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APPENDIX 7a

## EXPLANATION OF TERMS USED IN CROSS CHECK SUMMARY

MEAN: SUM OF DATA ENTRIES DIVIDED BY THE NUMBER OF ENTRIES GIVES AVERAGE VALUE OF DATA

$$\text{MEAN} = \frac{\sum x_i}{N} = \bar{x}$$

STANDARD DEVIATION: GIVES THE AVERAGE DIFFERENCE BETWEEN THE INDIVIDUAL DATA ENTRIES AND THE MEAN.

COMPUTED BY SUBTRACTING A DATA ENTRY FROM THE MEAN AND SQUARING THE DIFFERENCE. THE SQUARED TERMS ARE ADDED TOGETHER AND THAT TOTAL IS DIVIDED BY THE NUMBER OF ENTRIES MINUS ONE. THE SQUARE ROOT OF THAT ANSWER IS THE S.D.

$$\text{S.D.} = \sqrt{\frac{\sum_{i=1}^N (x_i - \bar{x})^2}{N-1}}$$

VARIANCE: IS THE SQUARE OF THE STANDARD DEVIATION

$$\text{VAR.} = \frac{\sum_{i=1}^N (x_i - \bar{x})^2}{N-1}$$

PRECISION (IN PCT): IS A NORMALIZED VALUE OF THE STANDARD DEVIATION. IT ALLOWS YOU TO COMPARE THE SPREAD OF A SMALL NUMBER TO THE SPREAD OF A LARGE NUMBER IN A MEANINGFUL WAY.

COMPUTED BY DIVIDING THE STANDARD DEVIATION BY THE MEAN. IN THIS CASE PRECISION IS GIVEN IN PER CENT SO THE ANSWER IS MULTIPLIED BY 100.

$$\text{PREC.} = \frac{\text{S.D.}}{\text{MEAN}} \times 100$$

CVS AND ANALYTICAL UNITS CROSS CHECK  
HIGHLAND PARK ENGINEERING  
DEPARTMENT 5140  
EMISSION DEVELOPMENT TESTING

DATE: WEEK of 9/19/77  
 VEHICLE TESTED: 515, 360 CID, W AUTO. TRANS.  
 TSP INERTIA: 4000# W AC FACTOR  
 TEST TYPE: HOT 505 W FLYING START  
 ENGINEER: A. E. PACHAJA

MODAL TEST RESULTS

COMPONENT ANALYZED (in grams/mile)	METHOD OF ANALYSIS	ROLLS NUMBER							
		20	21	22	23	24	25	26	27
HYDROCARBONS	P.I.D.	B/D/M	.893 .947	.830 .831	.784 .817	.947 .973	.891 .885	.902 .896	1.057 1.005
CARBON MONOXIDE	N.D.I.R.		3.82 3.82	3.72 3.58	3.75 3.66	3.72 3.70	3.79 3.76	4.11 4.10	3.66 3.60
CARBON DIOXIDE	N.D.I.R.		735 754	726 733	752 744	730 731	749 740	776 770	746 737
OXIDES OF NITROGEN	CHIM.		.931 .941	.875 .874	.976 .919	.868 .876	.944 .874	1.016 .997	.966 .936
FUEL ECONOMY	CARBON BALANCE		11.93 11.63	12.08 11.97	11.67 11.80	12.01 12.00	11.71 11.85	11.30 11.39	11.75 11.90
DISTANCE	MODAL-BAG RATIO	B/D/M	3.578 3.579	3.562 3.564	3.572 3.573	3.574 3.575	3.567 3.561	3.543 3.543	3.564 3.564

COMMENTS: (1) ROLLS 20 unavailable due to dyno evaluation.

CVS AND ANALYTICAL UNITS CROSS CHECK  
HIGHLAND PARK ENGINEERING  
DEPARTMENT 5140  
EMISSION DEVELOPMENT TESTING

DATE: WEEK of 9/19/77  
 VEHICLE TESTED: 515, 360 CID V AUTO TRANS.  
 TEST INERTIA: 4000# V AC FACTOR

COMPONENT ANALYZER (g/mi)		MEAN	VARIANCE	S, STD. DEV.	REPEATABILITY	MEAN-2S	MEAN+2S
HYDROCARBONS	MODAL BAG	.904 .688	.006 .002	.076 .039	* 8.43% * 5.69%	.752 .609	1.057 .766
CARBON MONOXIDE	MODAL BAG	3.771 3.740	.025 .017	.159 .129	4.22% 3.44%	3.452 3.482	4.089 3.998
CARBON DIOXIDE	MODAL BAG	744.5 735.8	218.9 139.7	14.8 11.8	1.99% 1.61%	714.9 712.2	774.1 759.4
OXIDES OF NITROGEN	MODAL BAG	.928 1.264	.002 .006	.049 .079	5.33% 6.28%	.829 1.106	1.027 1.423
FUEL ECONOMY	MODAL BAG	11.79 11.93	.03 .04	.23 .19	1.96% 1.58%	11.32 11.56	12.25 12.31
DISTANCE		3.566	.000	.011	0.32%	3.543	3.588

COMMENTS: (1) Repeatability for both bag and modal results are within the limits set forth in the Chrysler performance standard No. PP-6168 procedure No. LP 461 K 123, except modal and bag HC.

(2) Asterisk denotes out of spec.

CVS AND ANALYTICAL UNITS CROSS CHECK  
HIGHLAND PARK ENGINEERING  
DEPARTMENT 5140  
EMISSION DEVELOPMENT TESTING

DATE: WEEK of 9/19/77  
 VEHICLE TESTED: 515, 360 CID, V AUTO. TRANS.  
 TEST INERTIA: 4000# V AC FACTOR  
 TEST TYPE: HOT SOH V FLYING START  
 ENGINEER: A. E. PACHAMA

BAG TEST RESULTS

COMPONENT ANALYZED (in grams/mile)	METHOD OF ANALYSIS	ROLLS NUMBER							
		20	21	22	23	24	25	26	27
HYDROCARBONS	F.I.D.	DOWN	.703 .737	.634 .628	.646 .652	.712 .711	.690 .718	.681 .656	.705 .754
CARBON MONOXIDE	N.D.I.R.		3.84 3.78	3.80 3.62	3.70 3.61	3.60 3.77	3.61 3.65	3.93 4.03	3.72 3.70
CARBON DIOXIDE	N.D.I.R.		743.5 743.1	722.5 730.1	726.4 726.9	726.2 731.8	735.5 731.2	762.0 757.4	735.5 729.2
OXIDES OF NITROGEN	CHEM.		1.353 1.398	1.180 1.172	1.301 1.233	1.190 1.212	1.219 1.149	1.318 1.313	1.345 1.318
FUEL ECONOMY	CARBON BALANCE		11.81 11.81	12.15 12.03	12.09 12.08	12.09 11.99	11.94 12.01	11.52 11.59	11.94 12.04
	MODAL-BAG RATIO	DOWN							

COMMENTS: (1) ROLLS 20 UNAVAILABLE DUE TO DYNOMETER EVALUATION.

CVS AND ANALYTICAL UNITS CROSSCHECK  
CHELSEA PROVING GROUNDS  
DEPARTMENT 5150  
VEHICLE CERTIFICATION

DATE : September 26 and 27, 1977  
 VEHICLE TESTED: 855 (318 automatic w/catalyst)  
 TEST INERTIA : 4000#  
 TEST TYPE : Hot 505 w/flying start  
 ENGINEER : T. Kueny

BAG DATA

COMPONENT ANALYZED (in grams/mile)	METHOD OF ANALYSIS	ROLLS NUMBER							
		1	2	3	4	5	6	7	8
HYDROCARBONS	F.I.D.	.272	.300	.290	.334	.309	.285	.288	.317
CARBON MONOXIDE	N.D.I.R.	3.06	3.84	4.03	4.35	3.65	3.11	4.02	4.54
CARBON DIOXIDE	N.D.I.R.	554	559	550	561	553	558	559	563
OXIDES OF NITROGEN	CHEM.	1.76	1.84	1.79	1.95	1.79	1.89	1.90	2.01
FUEL ECONOMY	CARBON BALANCE	15.85	15.68	15.93	15.61	15.86	15.75	15.68	15.55
DISTANCE	DIGITAL COUNTER	3.58	3.56	3.60	3.60	3.58	3.59	3.60	3.59

- COMMENTS: 1) All tests were driven by the same person.  
 2) Cells 1 and 5 were tested on September 27; all other rolls were tested September 26  
 3) Chrysler Laboratory Procedure LP-461K-123 was followed with the exception that single tests were obtained from each cell instead of the prescribed duplicates.

CVS AND ANALYTICAL UNITS CROSSCHECK  
CHELSEA PROVING GROUNDS  
DEPARTMENT 5150  
VEHICLE CERTIFICATION

DATE : September 26, 1977  
 VEHICLE TESTED: 855 (318 automatic w/catalyst)  
 TEST INERTIA : 4000#  
 TEST TYPE : Hot 505 w/flying start  
 ENGINEER : T. Kueny

MODAL DATA

COMPONENT ANALYZED (in grams/mile)	METHOD OF ANALYSIS	ROLLS NUMBER							
		1	2	3	4	5	6	7	8
HYDROCARBONS	F.I.D.	.283	.410	.332	.329	.338	.296	.300	.327
CARBON MONOXIDE	N.D.I.R.	2.14	2.48	2.74	2.81	2.49	2.22	2.66	3.29
CARBON DIOXIDE	N.D.I.R.	564	567	563	566	567	561	564	569
OXIDES OF NITROGEN	CHEM.	1.65	1.75	1.74	1.90	1.76	1.86	1.86	2.02
FUEL ECONOMY	CARBON BALANCE	15.61	15.50	15.61	15.53	15.51	15.68	15.59	15.43
EXHAUST VOLUME	MODAL-BAG RATIO	324	317	316	336	319	311	317	341

- COMMENTS: 1) Modal hydrocarbons from rolls 2 are excessively high with respect to both other rolls and to bag results. Analyzer shift is suspected but the overall system will be investigated.  
 2) Both exhaust volume and CO<sub>2</sub> data are high for the second consecutive week on rolls #4.

CVS AND ANALYTICAL UNITS CROSS CHECK  
HIGHLAND PARK ENGINEERING  
DEPARTMENT 5150  
EMISSION DEVELOPMENT TESTING

DATE: September 26, 1977  
 VEHICLE TESTED: 855 (318 automatic w/catalyst)  
 TEST INERTIA: 4000#

COMPONENT ANALYZER(g/mi.)		MEAN	VARIANCE	S, STD. DEV.	REPEATABILITY%	MEAN-2S	MEAN+2S
HYDROCARBONS	MODAL	.327	.0015	.039	11.9	.249	.405
	BAG	.299	.0004	.020	6.7	.260	.339
CARBON MONOXIDE	MODAL	2.60	.132	.36	14.0	1.88	3.33
	BAG	3.83	.285	.53	14.0	2.76	4.89
CARBON DIOXIDE	MODAL	565	6.70	2.6	.5	560	570
	BAG	557	19.3	4.4	.8	548	566
OXIDES OF NITROGEN	MODAL	1.82	.0133	.115	6.4	1.59	2.05
	BAG	1.87	.0076	.087	4.7	1.69	2.04
FUEL ECONOMY	MODAL	15.56	.01	.08	.5	15.40	15.72
	BAG	15.74	.02	.13	.8	15.47	16.00
EXHAUST VOLUME	MODAL CALC.	323	111	10.5	3.3	302	344

- COMMENTS: 1) According to Chrysler Performance Standard PP-6168, maximum allowable percent variation for a vehicle omitting at these levels is 10% HC, 15% CO, 10% NO<sub>x</sub> and 3% CO<sub>2</sub>. Only modal hydrocarbons exceed this limit and is denoted with an asterisk.  
 2) Modal-bag agreement for CO<sub>2</sub>, NO<sub>x</sub> and fuel economy is excellent; agreement for HC and CO is poor but is influenced by the low emissions levels measured.

# CORRELATION VEHICLES

EPA I-1

- A. BOTH SMALL AND LARGE ARE DESIRABLE.
- B. SET SCHEDULE FOR SITES AND DEVELOP A BASELINE.
- C. MONITOR COAST DOWN  $\Delta t$ 'S AFTER TEST.
- D. PLOT DATA AND DO STATISTICS FOR ONE MONTH PERIOD (40 TESTS)  
(EXAMPLE 2 TESTS/DAY  $\times$  20 DAYS  $\div$  8 SITES = 5/SITE)

APPENDIX 7B

Don PAULSELL EPA

DB	WB	H	Kh	% $\Delta$
74	64	75.2	1.001	0
73	63	72.0	.986	-1.5
72	62	68.9	.972	-2.9
71	61	65.9	.959	-4.2

BARO = 29.0"

EFFECT OF ERROR IN TEMPERATURE MEASUREMENT  
FOR SAME " $\Delta T$ "

SHED SYSTEM

<u>QC CHECK</u>	<u>TECHNIQUE</u>	<u>FREQUENCY</u>	<u>ACCURACY</u>
1. SHED Volume	Propane Injection	At Introduction	+ - 2%
2. SHED Background	4 Hour Check	Yearly	.4 gm max
3. SHED Leakage	Propane Injection	Monthly	4% in 4 hours

# SHED SYSTEM

## General

- M-VEL Designed

- Enclosure
- Console
- Cooling System

- Enclosure

- "Guillotine" Style Door.
- Pneumatic Door Seal
- Two - 420 cfm Centrifugal Blowers
- Medium and High Volume SHEDS

- Console

- "State of the Art" Components
- Computer Interface Capability
- Manual Diurnal Heating
- High Level Signal Conditioning
- Self-Contained Diagnostic Devices
- "Prom" Type - System Controller

- Cooling System

- Internally Mounted Cooling System
- Closed-Loop Servo Controlled
- Water-to-Water Heat Exchanger
- Manual Override Capabilities

# IN-PROCESS QC TECHNIQUES

- A. CALIBRATION GAS MONITORING
- B. DVU HORSEPOWER CHECK OF ARLC
- C. TEST DATA RATIOS AND LIMITS
  - VMIX 2/1 AND 1/3
  - CO<sub>2</sub> BAG X/TOTAL GMS
  - BKGD LEVELS
  - NOX-KH
  - RPM RATIO FOR PDP-CVS