

**Arsenic Removal from Drinking Water by Iron Removal  
EPA Demonstration Project at  
Big Sauk Lake Mobile Home Park in Sauk Centre, MN  
Six-Month Evaluation Report**

by

**H. Tien Shiao  
Abraham S.C. Chen  
Wendy E. Condit  
Lili Wang**

**Battelle  
Columbus, OH 43201-2693**

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**Thomas J. Sorg  
Task Order Manager**

**Water Supply and Water Resources Division  
National Risk Management Research Laboratory  
Cincinnati, Ohio 45268**

**National Risk Management Research Laboratory  
Office of Research and Development  
U.S. Environmental Protection Agency  
Cincinnati, Ohio 45268**

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Sally Gutierrez, Director  
National Risk Management Research Laboratory

## ABSTRACT

This report documents the activities performed and the results obtained from the first six months of the arsenic removal treatment technology demonstration project at the Big Sauk Lake Mobile Home Park (BSLMHP) in Sauk Centre, MN. The objectives of the project are to evaluate the effectiveness of Kinetico's Macrolite<sup>®</sup> pressure filtration process in removing arsenic to meet the new arsenic maximum contaminant level (MCL) of 10 µg/L, the reliability of the treatment system, the required system operation and maintenance (O&M) and operator skill levels, and the capital and O&M cost of the technology. The project also is characterizing water in the distribution system and process residuals produced by the treatment system.

The Macrolite<sup>®</sup> CP-213f arsenic removal system at BSLMHP consisted of two 36-in diameter by 57-in tall contact tanks (205 gal each) and four 13-in diameter by 54-in tall pressure tanks (two for each duplex unit), all configured in parallel. Each pressure tank contained 20 in (or 1.5 ft<sup>3</sup>) of Macrolite<sup>®</sup> filter media. The maximum design flowrate was 20 gpm, which yielded at least 20 min of contact time prior to pressure filtration and at least 5.4 gpm/ft<sup>2</sup> of hydraulic loading to the Macrolite<sup>®</sup> filters. Because the system operated in an on-demand configuration, the actual flowrates ranged from 1 to 15 gpm, corresponding to 27 to 410 min of contact time and 0.3 to 4.1 gpm/ft<sup>2</sup> of hydraulic loading. From July 13, 2005, through January 17, 2006, the system operated for a total of 617 hr at approximately 3.4 hr/day. Based on the totalizer readings, the system treated approximately 863,470 gal of water with an average daily demand of 4,617 gal during this time period.

Total arsenic concentrations in source water ranged from 20.6 to 36.6 µg/L with As(III) being the predominating species at an average concentration of 23.0 µg/L. Potassium permanganate (KMnO<sub>4</sub>) was used to oxidize As(III) and Fe(II) prior to Macrolite<sup>®</sup> pressure filtration. KMnO<sub>4</sub> was selected as the oxidant because of the presence of elevated total organic carbon (TOC) levels (at 3.2 to 4.8 mg/L) in source water and high formation potential of disinfection byproducts with the use of chlorine.

After the contact tanks, As(III) concentrations were reduced to an average value of 1.9 µg/L, suggesting effective oxidation of As(III) to As(V) with KMnO<sub>4</sub>. Meanwhile, arsenic was present primarily in the particulate form at an average value of 22.9 µg/L, presumably, by being bound to iron particles. During the first six months from July 13, 2005, through January 17, 2006, total arsenic levels in the treated water were reduced to 2.9 to 17.7 µg/L (averaged 7.6 µg/L). Out of 24 sampling occasions, arsenic concentrations exceeded the 10-µg/L MCL for a total of eight times, with all but one due to particulate breakthrough. Two samples exceeded total arsenic concentrations of 10 µg/L due to low KMnO<sub>4</sub> dosage, resulting in incomplete oxidation of As(III) and Fe(II). In order to address particulate arsenic breakthrough, the backwash frequency was increased from every 2,743 gal to every 1,714 gal of throughput during this time period.

Total iron concentrations averaged 2,760 µg/L in source water, which is above the secondary MCL of 300 µg/L. With an average soluble iron to soluble arsenic ratio of 100:1, there was sufficient natural iron present in source water for effective arsenic removal. After the contact tanks, iron was present primarily in the particulate form, suggesting effective oxidation even in the presence of elevated TOC levels. Total iron concentrations in the treated water ranged from <25 to 1,067 µg/L and averaged 259 µg/L. An increase in particulate iron correlated with an increase in particulate arsenic, indicating iron breakthrough from the Macrolite<sup>®</sup> filters.

Total manganese concentrations averaged 144 µg/L in source water, existing primarily in the soluble form as Mn(II) at 132 µg/L. After the addition of 2.6 to 3.8 mg/L of KMnO<sub>4</sub> and after the contact tanks, manganese was present primarily in the soluble form based on the use of 0.45-µm disc filters, with levels

ranging from 337 to 946 µg/L before November 15, 2005. The high levels of TOC in source water appeared to have inhibited the formation of filterable manganese solids. Based on the results of a series of jar tests, the KMnO<sub>4</sub> dosage applied to the treatment system was increased to 5.6 mg/L. The increased KMnO<sub>4</sub> dosage enabled most manganese to precipitate after the contact tanks, leaving only 108 to 166 µg/L measured as soluble manganese. Further adjustments will be made to the KMnO<sub>4</sub> dosing in the next six-month period to further lower the soluble manganese levels.

During this time period, the backwash water production rates ranged from 2.8 to 7.2%. The control disc on top of each set of duplex units was changed out twice to increase the backwash frequency in order to address the particulate arsenic, iron, and manganese breakthrough. The backwash frequency was increased from the initial field setting of every 2,743 gal to every 1,714 gal. If needed, further adjustments will be made in the next six-month study period. After November 15, 2006, when the modified backwash procedure was implemented, total arsenic concentrations in the backwash water ranged from 114 to 417 µg/L; total iron concentrations ranged from 14,069 to 77,641 µg/L; and total manganese concentrations ranged from 1,595 to 16,178 µg/L. Using 130 gal of backwash water produced, this equates to approximately 0.17 lb of solids, including  $4.4 \times 10^{-4}$  lb of arsenic, 0.08 lb of iron, and 0.01 lb manganese, generated per backwash event.

Comparison of the distribution system sampling results before and after system startup showed a significant decrease in arsenic and iron levels and a significant increase in manganese levels at all three sampling locations. The distribution water sampling results essentially mirrored the treatment results of the Macrolite<sup>®</sup> filters. Neither lead nor copper concentrations at the sample sites appear to have been affected by the operation of the system.

The capital investment cost was \$63,547, which included \$22,422 for equipment, \$20,227 for engineering, and \$20,898 for installation. Using the system's rated capacity of 20 gal/min (gpm) (28,800 gal/day [gpd]), the capital cost was \$3,177/gpm (\$2.21/gpd).

The O&M cost for the Macrolite<sup>®</sup> CP-213f system included only incremental cost associated with the chemical supply, electricity consumption, and labor. The O&M cost was estimated in this report at \$0.43/1,000 gal and will be refined at the end of the one-year evaluation period.

# CONTENTS

DISCLAIMER .....	ii
FOREWORD .....	iii
ABSTRACT .....	iv
FIGURES .....	vii
TABLES .....	vii
ABBREVIATIONS AND ACRONYMS .....	ix
ACKNOWLEDGMENTS .....	xi
Section 1.0: INTRODUCTION .....	1
1.1 Treatment Technologies for Arsenic Removal .....	2
1.2 Project Objectives .....	2
Section 2.0: SUMMARY AND CONCLUSIONS .....	5
Section 3.0: MATERIALS AND METHODS .....	7
3.1 General Project Approach .....	7
3.2 System O&M and Cost Data Collection .....	8
3.3 Sample Collection Procedures and Schedules .....	8
3.3.1 Source Water .....	11
3.3.2 Treatment Plant Water .....	11
3.3.3 Special Study - KMnO <sub>4</sub> Jar Tests .....	11
3.3.4 Backwash Water .....	11
3.3.5 Residual Solids .....	12
3.3.6 Distribution System Water .....	12
3.4 Sampling Logistics .....	12
3.4.1 Preparation of Arsenic Speciation Kits .....	12
3.4.2 Preparation of Sampling Coolers .....	12
3.4.3 Sample Shipping and Handling .....	12
3.5 Analytical Procedures .....	13
Section 4.0: RESULTS AND DISCUSSION .....	14
4.1 Facility Description and Pre-Existing Treatment System Infrastructure .....	14
4.1.1 Source Water Quality .....	14
4.1.2 Distribution System and Treated Water Quality .....	16
4.2 Treatment Process Description .....	17
4.3 System Installation .....	22
4.3.1 Permitting .....	22
4.3.2 Building Construction .....	22
4.3.3 System Installation, Shakedown, and Startup .....	22
4.4 System Operation .....	23
4.4.1 Operational Parameters .....	23
4.4.2 Backwash .....	23
4.4.3 Residual Management .....	25
4.4.4 System/Operation Reliability and Simplicity .....	25
4.5 System Performance .....	26
4.5.1 Treatment Plant Sampling .....	26
4.5.2 Backwash Water Sampling .....	37
4.5.3 Distribution System Water Sampling .....	38

4.6	System Cost .....	41
4.6.1	Capital Cost .....	41
4.6.2	Operation and Maintenance Cost .....	42
Section 5.0: REFERENCES .....		44
APPENDIX A: OPERATIONAL DATA .....		A-1
APPENDIX B: ANALYTICAL DATA .....		B-1

## FIGURES

Figure 3-1.	Process Flow Diagram and Sampling Locations.....	10
Figure 4-1.	Pre-Existing Pump House at BSLMHP, MN Site.....	14
Figure 4-2.	Existing Well Piping and Pressure Tanks at BSLMHP, MN Site.....	15
Figure 4-3.	Process Schematic of Macrolite® Pressure Filtration System .....	18
Figure 4-4.	Photograph of Macrolite® Pressure Filtration System .....	18
Figure 4-5.	KMnO <sub>4</sub> Feed System.....	20
Figure 4-6.	Kinetico's Mach 1250 Control Valve .....	20
Figure 4-7.	Backwash Flow Path for One Duplex Unit with Control Disc No. 8 and a Throughput of 1,714 gal between Backwash Cycles .....	21
Figure 4-8.	Concentrations of Arsenic Species at IN, AC, and TT Sampling Locations .....	30
Figure 4-9.	Total Arsenic Concentrations at TA/TB, TC/TD, and TT Sampling Locations .....	31
Figure 4-10.	Total Iron Concentrations at TA/TB, TC/TD, and TT Sampling Locations .....	31
Figure 4-11.	Total and Soluble Manganese Concentrations at AC Sampling Location .....	33
Figure 4-12.	Total Manganese Concentrations at TA/TB, TC/TD, and TT Sampling Locations .....	34
Figure 4-13.	Jar Test Setup .....	36
Figure 4-14.	Total Phosphorous Concentrations at IN, AC, TA/TB, TC/TD and TT Sampling Locations.....	38

## TABLES

Table 1-1.	Summary of Round 1 and Round 2 Arsenic Removal Demonstration Locations, Technologies, and Source Water Quality.....	3
Table 3-1.	Predemonstration Study Activities and Completion Dates .....	7
Table 3-2.	Evaluation Objectives and Supporting Data Collection Activities .....	7
Table 3-3.	Sample Collection Schedule and Analyses .....	9
Table 3-4.	Summary of Jar Test Parameters.....	11
Table 4-1.	BSLMHP, MN Water Quality Data .....	16
Table 4-2.	Physical Properties of M2 Macrolite® Media.....	17
Table 4-3.	Design Specifications for Macrolite® CP-213f Pressure Filtration System .....	19
Table 4-4.	System Operation from July 13, 2005 to January 17, 2006 .....	24
Table 4-5.	Control Disc Size and Throughput between Backwash Cycles .....	25
Table 4-6.	Summary of Arsenic, Iron, and Manganese Analytical Results.....	27
Table 4-7.	Summary of Other Water Quality Parameter Sampling Results.....	28
Table 4-8.	Control Disc Sizes and Corresponding Occurrences with High Total Arsenic and Iron Concentrations.....	32

Table 4-9.	Correlations Between Pump Stroke Length, $\text{KMnO}_4$ Dosage, and Total and Soluble Manganese Concentrations .....	33
Table 4-10.	Jar Test Results for Macrolite <sup>®</sup> -Treated Water .....	35
Table 4-11.	Backwash Water Sampling Results .....	39
Table 4-12.	Distribution Sampling Results .....	40
Table 4-13.	Summary of Capital Investment for BSLMHP Treatment System.....	42
Table 4-14.	O&M Cost for BSLMHP, MN Treatment System.....	43

## ABBREVIATIONS AND ACRONYMS

AAL	American Analytical Laboratories
Al	aluminum
AM	adsorptive media
As	arsenic
BSLMHP	Big Sauk Lake Mobile Home Park
BTU-hr	British Thermal Units per hour
Ca	calcium
Cu	copper
DO	dissolved oxygen
DOM	dissolved organic matter
EPA	U.S. Environmental Protection Agency
F	fluoride
Fe	iron
FRP	fiberglass reinforced plastic
GFH	granular ferric hydroxide
gpd	gallons per day
gpm	gallons per minute
HDPE	high-density polyethylene
hp	horsepower
ICP-MS	inductively coupled plasma-mass spectrometry
ID	identification
IX	ion exchange
LCR	Lead and Copper Rule
MCL	maximum contaminant level
MDL	method detection limit
MDH	Minnesota Department of Health
Mg	magnesium
Mn	manganese
Mo	molybdenum
mV	millivolts
Na	sodium
NA	not applicable
NaOCl	sodium hypochlorite
NRMRL	National Risk Management Research Laboratory
NTU	nephelometric turbidity units
O&M	operation and maintenance

OIT	Oregon Institute of Technology
ORD	Office of Research and Development
ORP	oxidation-reduction potential
PE	professional engineer
P&ID	pipng and instrumentation diagrams
POU	point-of-use
psi	pounds per square inch
PVC	polyvinyl chloride
QA	quality assurance
QAPP	quality assurance project plan
QA/QC	quality assurance/quality control
RO	reverse osmosis
RPD	relative percent difference
Sb	antimony
SDWA	Safe Drinking Water Act
SMCL	Secondary Maximum Contaminant Level
TBD	to be determined
TCLP	Toxicity Characteristic Leaching Procedure
TDS	total dissolved solids
TOC	total organic carbon
TSS	total suspended solids
TTHM	total trihalomethane
V	vanadium

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## 1.0: INTRODUCTION

The Safe Drinking Water Act (SDWA) mandates that U.S. Environmental Protection Agency (EPA) identify and regulate drinking water contaminants that may have adverse human health effects and that are known or anticipated to occur in public water supply systems. In 1975 under the SDWA, EPA established a maximum contaminant level (MCL) for arsenic at 0.05 mg/L. Amended in 1996, the SDWA required that EPA develop an arsenic research strategy and publish a proposal to revise the arsenic MCL by January 2000. On January 18, 2001, EPA finalized the arsenic MCL at 0.01 mg/L (EPA, 2001). In order to clarify the implementation of the original rule, EPA revised the rule on March 25, 2003 to express the MCL as 0.010 mg/L (10 µg/L) (EPA, 2003). The final rule requires all community and non-transient, non-community water systems to comply with the new standard by January 23, 2006.

In October 2001, EPA announced an initiative for additional research and development of cost-effective technologies to help small community water systems (<10,000 customers) meet the new arsenic standard and to provide technical assistance to operators of small systems in order to reduce compliance costs. As part of this Arsenic Rule Implementation Research Program, EPA's Office of Research and Development (ORD) proposed a project to conduct a series of full-scale, on-site demonstrations of arsenic removal technologies, process modifications, and engineering approaches applicable to small systems. Shortly thereafter, an announcement was published in the *Federal Register* requesting water utilities interested in participating in Round 1 of this EPA-sponsored demonstration program to provide information on their water systems. In June 2002, EPA selected 17 out of 115 sites to be the host sites for the demonstration studies.

In September 2002, EPA solicited proposals from engineering firms and vendors for cost-effective arsenic removal treatment technologies for the 17 host sites. EPA received 70 technical proposals for the 17 host sites, with each site receiving one to six proposals. In April 2003, an independent technical panel reviewed the proposals and provided its recommendations to EPA on the technologies that it determined were acceptable for the demonstration at each site. Because of funding limitations and other technical reasons, only 12 of the 17 sites were selected for the demonstration project. Using the information provided by the review panel, EPA, in cooperation with the host sites and the drinking water programs of the respective states, selected one technical proposal for each site. As of February 2007, 11 of the 12 systems have been operational and the performance evaluation of six systems has been completed.

In 2003, EPA initiated Round 2 arsenic technology demonstration projects that were partially funded with Congressional add-on funding to the EPA budget. In June 2003, EPA selected 32 potential demonstration sites and the Big Sauk Lake Mobile Home Park (BSLMHP) in Sauk Centre, MN was one of them.

In September 2003, EPA, again solicited proposals from engineering firms and vendors for arsenic removal technologies. EPA received 148 technical proposals for the 32 host sites, with each site receiving from two to eight proposals. In April 2004, another technical panel was convened by EPA to review the proposals and provide recommendations to EPA with the number of proposals per site ranging from none (for two sites) to a maximum of four. The final selection of the treatment technology at the sites that received at least one proposal was made, again through a joint effort by EPA, the state regulators, and the host site. Since then, four sites have withdrawn from the demonstration program, reducing the number of sites to 28. Kinetico's Macrolite® Arsenic Removal Technology was selected for demonstration at the BSLMHP site.

## **1.1 Treatment Technologies for Arsenic Removal**

The technologies selected for the Round 1 and Round 2 demonstration host sites include 25 adsorptive media (AM) systems (the Oregon Institute of Technology [OIT] site has three AM systems), 13 coagulation/filtration (C/F) systems, two ion exchange (IX) systems, and 17 point-of-use (POU) units (including nine under-the-sink reverse osmosis [RO] units at the Sunset Ranch Development site and eight AM units at the OIT site), and one system modification. Table 1-1 summarizes the locations, technologies, vendors, system flowrates, and key source water quality parameters (including As, Fe, and pH) at the 40 demonstration sites. An overview of the technology selection and system design for the 12 Round 1 demonstration sites and the associated capital costs is provided in two EPA reports (Wang et al., 2004 and Chen et al., 2004), which are posted on the EPA website at <http://www.epa.gov/ORD/NRMRL/wswrd/dw/arsenic/index.html>.

## **1.2 Project Objectives**

The objective of the Round 1 and Round 2 arsenic demonstration program is to conduct 40 full-scale arsenic treatment technology demonstration studies on the removal of arsenic from drinking water supplies. The specific objectives are to:

- Evaluate the performance of the arsenic removal technologies for use on small systems.
- Determine the required system operation and maintenance (O&M) and operator skill levels.
- Characterize process residuals produced by the technologies.
- Determine the capital and O&M cost of the technologies.

This report summarizes the performance of the Kinetico Macrolite<sup>®</sup> CP-213f arsenic removal system at BSLMHP in Sauk Centre, MN from July 13, 2005, through January 17, 2006. The types of data collected included system operation, water quality (both across the treatment train and in the distribution system), residuals, and capital and preliminary O&M cost.

**Table 1-1. Summary of Round 1 and Round 2 Arsenic Removal Demonstration Locations, Technologies, and Source Water Quality**

Demonstration Location	Site Name	Technology (Media)	Vendor	Design Flowrate (gpm)	Source Water Quality		
					As (µg/L)	Fe (µg/L)	pH (S.U.)
<i>Northeast/Ohio</i>							
Wales, ME	Springbrook Mobile Home Park	AM (A/I Complex)	ATS	14	38 <sup>(a)</sup>	<25	8.6
Bow, NH	White Rock Water Company	AM (G2)	ADI	70 <sup>(b)</sup>	39	<25	7.7
Goffstown, NH	Orchard Highlands Subdivision	AM (E33)	AdEdge	10	33	<25	6.9
Rollinsford, NH	Rollinsford Water and Sewer District	AM (E33)	AdEdge	100	36 <sup>(a)</sup>	46	8.2
Dummerston, VT	Charette Mobile Home Park	AM (A/I Complex)	ATS	22	30	<25	7.9
Felton, DE	Town of Felton	C/F (Macrolite)	Kinetico	375	30 <sup>(a)</sup>	48	8.2
Stevensville, MD	Queen Anne's County	AM (E33)	STS	300	19 <sup>(a)</sup>	270 <sup>(c)</sup>	7.3
Houghton, NY <sup>(d)</sup>	Town of Caneadea	C/F (Macrolite)	Kinetico	550	27 <sup>(a)</sup>	1,806 <sup>(c)</sup>	7.6
Newark, OH	Buckeye Lake Head Start Building	AM (ARM 200)	Kinetico	10	15 <sup>(a)</sup>	1,312 <sup>(c)</sup>	7.6
Springfield, OH	Chateau Estates Mobile Home Park	AM (E33)	AdEdge	250 <sup>(e)</sup>	25 <sup>(a)</sup>	1,615 <sup>(c)</sup>	7.3
<i>Great Lakes/Interior Plains</i>							
Brown City, MI	City of Brown City	AM (E33)	STS	640	14 <sup>(a)</sup>	127 <sup>(c)</sup>	7.3
Pentwater, MI	Village of Pentwater	C/F (Macrolite)	Kinetico	400	13 <sup>(a)</sup>	466 <sup>(c)</sup>	6.9
Sandusky, MI	City of Sandusky	C/F (Aeralater)	Siemens	340 <sup>(e)</sup>	16 <sup>(a)</sup>	1,387 <sup>(c)</sup>	6.9
Delavan, WI	Vintage on the Ponds	C/F (Macrolite)	Kinetico	40	20 <sup>(a)</sup>	1,499 <sup>(c)</sup>	7.5
Greenville, WI	Town of Greenville	C/F (Macrolite)	Kinetico	375	17	7827 <sup>(c)</sup>	7.3
Climax, MN	City of Climax	C/F (Macrolite)	Kinetico	140	39 <sup>(a)</sup>	546 <sup>(c)</sup>	7.4
Sabin, MN	City of Sabin	C/F (Macrolite)	Kinetico	250	34	1,470 <sup>(c)</sup>	7.3
Sauk Centre, MN	Big Sauk Lake Mobile Home Park	C/F (Macrolite)	Kinetico	20	25 <sup>(a)</sup>	3,078 <sup>(c)</sup>	7.1
Stewart, MN	City of Stewart	C/F&AM (E33)	AdEdge	250	42 <sup>(a)</sup>	1,344 <sup>(c)</sup>	7.7
Lidgerwood, ND	City of Lidgerwood	Process Modification	Kinetico	250	146 <sup>(a)</sup>	1,325 <sup>(c)</sup>	7.2
<i>Midwest/Southwest</i>							
Arnaudville, LA	United Water Systems	C/F (Macrolite)	Kinetico	770 <sup>(e)</sup>	35 <sup>(a)</sup>	2,068 <sup>(c)</sup>	7.0
Alvin, TX	Oak Manor Municipal Utility District	AM (E33)	STS	150	19 <sup>(a)</sup>	95	7.8
Bruni, TX	Webb Consolidated Independent School District	AM (E33)	AdEdge	40	56 <sup>(a)</sup>	<25	8.0
Wellman, TX	City of Wellman	AM (E33)	AdEdge	100	45	<25	7.7
Anthony, NM	Desert Sands Mutual Domestic Water Consumers Association	AM (E33)	STS	320	23 <sup>(a)</sup>	39	7.7
Nambe Pueblo, NM	Nambe Pueblo Reservation	AM (E33)	AdEdge	145	33	<25	8.5
Taos, NM	Town of Taos	AM (E33)	STS	450	14	59	9.5
Rimrock, AZ	Arizona Water Company	AM (E33)	AdEdge	90 <sup>(b)</sup>	50	170	7.2
Tohono O'odham Nation, AZ	Tohono O'odham Utility Authority	AM (E33)	AdEdge	50	32	<25	8.2
Valley Vista, AZ	Arizona Water Company	AM (AAFS50/ARM 200)	Kinetico	37	41	<25	7.8

**Table 1-1. Summary of Round 1 and Round 2 Arsenic Removal Demonstration Locations, Technologies, and Source Water Quality (Continued)**

Demonstration Location	Site Name	Technology (Media)	Vendor	Design Flowrate (gpm)	Source Water Quality		
					As (µg/L)	Fe (µg/L)	pH
<i>Far West</i>							
Three Forks, MT	City of Three Forks	C/F (Macrolite)	Kinetico	250	64	<25	7.5
Fruitland, ID	City of Fruitland	IX (A300E)	Kinetico	250	44	<25	7.4
Homedale, ID	Sunset Ranch Development	POU RO <sup>(f)</sup>	Kinetico	75 gpd	52	134	7.5
Okanogan, WA	City of Okanogan	C/F (Electromedia-I)	Filtronics	750	18	69 <sup>(c)</sup>	8.0
Klamath Falls, OR	Oregon Institute of Technology	POE AM (Adsorbisia/ARM 200/ArsenX <sup>np</sup> ) and POU AM (ARM 200) <sup>(g)</sup>	Kinetico	60/60/30	33	<25	7.9
Vale, OR	City of Vale	IX (Arsenex II)	Kinetico	525	17	<25	7.5
Reno, NV	South Truckee Meadows General Improvement District	AM (GFH)	Siemens	350	39	<25	7.4
Susanville, CA	Richmond School District	AM (A/I Complex)	ATS	12	37 <sup>(a)</sup>	125	7.5
Lake Isabella, CA	Upper Bodfish Well CH2-A	AM (HIX)	VEETech	50	35	125	7.5
Tehachapi, CA	Golden Hills Community Service District	AM (Isolux)	MEI	150	15	<25	6.9

AM = adsorptive media process; C/F = coagulation/filtration; HIX = hybrid ion exchanger; IX = ion exchange process; RO = reverse osmosis

ATS = Aquatic Treatment Systems; MEI = Magnesium Elektron, Inc.; STS = Severn Trent Services

(a) Arsenic existing mostly as As(III).

(b) Design flowrate reduced by 50% due to system reconfiguration from parallel to series operation.

(c) Iron existing mostly as Fe(II).

(d) Replaced Village of Lyman, NE site which withdrew from program in June 2006.

(e) Facilities upgraded systems in Springfield, OH from 150 to 250 gpm, Sandusky, MI from 210 to 340 gpm, and Arnaudville, LA from 385 to 770 gpm.

(f) Including nine residential units.

(g) Including eight under-the-sink units.

## Section 2.0: SUMMARY AND CONCLUSIONS

Based on the information collected during the first six months of system operation, the following conclusions were made relating to the overall objectives of the treatment technology demonstration study.

*Performance of the arsenic removal technology for use on small systems:*

- $\text{KMnO}_4$ , selected over chlorine due to the presence of elevated total organic carbon (TOC) levels (i.e., 3.2 to 4.8 mg/L) and high formation potential of disinfection byproducts in source water, was effective in oxidizing As (III), reducing its concentrations from an average of 23  $\mu\text{g/L}$  to an average of 1.9  $\mu\text{g/L}$  after the contact tanks. Arsenic after the contact tanks was converted mostly to particulate arsenic, which was ready to be removed by the Macrolite<sup>®</sup> filters.  $\text{KMnO}_4$  also was effective in oxidizing soluble iron despite the presence of high TOC levels in raw water.
- Even at significantly reduced loading rates of 0.3 to 4.1 gpm/ft<sup>2</sup>, the Macrolite<sup>®</sup> filters did not consistently remove arsenic to the 10- $\mu\text{g/L}$  level. The removal at the target level was achieved during only 16 of the 24 weekly sampling events. Breakthrough of particulate arsenic and iron at concentrations as high as 21.5 and 2,363  $\mu\text{g/L}$ , respectively, from the Macrolite<sup>®</sup> filters was the main reason for not meeting the target arsenic MCL.
- Because of the observed particulate breakthrough, the filter backwash frequency had to be repeatedly increased from the initial field setting of once every 2,743 gal to once every 1,714 gal during the first six-month study period. As a result, the backwash water generation ratios were increased correspondingly from 5.5 to 7.2%. Further adjustments to the backwash frequency will have to be implemented during the next six-month study period because of continuing particulate breakthrough.
- Oxidation of Mn(II) with  $\text{KMnO}_4$  was affected by the presence of dissolved organic matter (DOM) in raw water, forming fine colloidal particles not retainable by 0.45- $\mu\text{m}$  disc filters. A dosage of at least 4.58 mg/L appeared to be needed to form filterable manganese solids, thus reducing the “soluble” manganese levels, as measured by using 0.45- $\mu\text{m}$  disc filters, from as high as 946  $\mu\text{g/L}$  to below 166  $\mu\text{g/L}$  after the contact tanks.
- Elevated total phosphorous levels ranging from 0.4 to 0.6 mg/L (as P) were detected in raw water. Total phosphorous existed primarily as total hydrolysable phosphorous, including polyphosphorous and some organic phosphorous according to EPA Method 365.4. No organopesticides, however, were present in source water according the EPA Method 507. Potential sources of elevated phosphorous included non-point source discharge from septic systems, agriculture, and urban runoff.

The Macrolite<sup>®</sup> filtration process was able to remove about 80% of total phosphorous.

*Simplicity of required system O&M and operator skill levels:*

- The daily demand on the operator was about 5 min, which included performing O&M activities such as mixing the  $\text{KMnO}_4$  solution, measuring the  $\text{KMnO}_4$  consumption, installing the hour meter, and working with the vendor to troubleshoot and perform minor on-site repairs.

- The system experienced some operational issues, which were related primarily to the backwash frequency. The throughput between backwash cycles had to be reduced repeatedly by using different control discs installed on top of the duplex units.
- There was no significant downtime during the first six months of system operation. However, the primary well pump developed a leak on January 4, 2006, which was repaired within a day. Further, a backwash malfunction occurred on August 9, 2005, which necessitated repairs by the vendor.

*Process residuals produced by the technology:*

- Based on the average of samples taken during several backwash events, the amount of solids produced per backwash event was 0.17 lb, which was composed of approximately 0.08 lb of iron and  $4.4 \times 10^{-4}$  lb of arsenic.

*Cost-effectiveness of the technology:*

- Using the system's rated capacity of 20 gal/min (gpm) (or 28,800 gal/day [gpd]), the capital cost was \$3,177 per gpm (or \$2.21 per gpd). The unit capital cost was \$0.57/1,000 gal if the system operated at 100% utilization rate. The system's real unit cost was 3.47/1,000 gal, based on 3.4 hr/day of system operation and 863,470 of water production.
- The O&M cost was \$0.43/1000 gal, based on labor, chemical usage, and electricity consumption.

### 3.0: MATERIALS AND METHODS

#### 3.1 General Project Approach

Following the pre-demonstration activities summarized in Table 3-1, the performance evaluation of the Macrolite<sup>®</sup> treatment system began on July 13, 2005. Table 3-2 summarizes the types of data collected and/or considered as part of the technology evaluation process. The overall system performance was evaluated based on its ability to consistently remove arsenic to below the target MCL of 10 µg/L through the collection of water samples across the treatment train. The reliability of the system was evaluated by tracking the unscheduled system downtime and frequency and extent of repair and replacement. The unscheduled downtime and repair information were recorded by the plant operator on a Repair and Maintenance Log Sheet.

**Table 3-1. Predemonstration Study Activities and Completion Dates**

Activity	Date
Introductory Meeting Held	08/31/04
Request for Quotation Issued to Vendor	12/06/04
Vendor Quotation Received	02/17/05
Purchase Order Established	02/24/05
Letter of Understanding Issued	01/10/05
Letter Report Issued	03/09/05
Engineering Package Submitted to MDH	03/28/05
Permit Granted by MDH	06/14/05
Study Plan Issued	06/21/05
Macrolite <sup>®</sup> Unit Shipped	06/10/05
Macrolite <sup>®</sup> Unit Delivered	06/16/05
System Installation Completed	06/24/05
System Shakedown Completed	07/03/05
Performance Evaluation Begun	07/13/05

MDH = Minnesota Department of Health

**Table 3-2. Evaluation Objectives and Supporting Data Collection Activities**

Evaluation Objective	Data Collection
Performance	-Ability to consistently meet 10 µg/L of arsenic in treated water
Reliability	-Unscheduled system downtime -Frequency and extent of repairs including a description of problems, materials and supplies needed, and associated labor and cost
System O&M and Operator Skill Requirements	-Pre- and post-treatment requirements -Level of automation for system operation and data collection -Staffing requirements including number of operators and laborers -Task analysis of preventive maintenance including number, frequency, and complexity of tasks -Chemical handling and inventory requirements -General knowledge needed for relevant chemical processes and health and safety practices
Residual Management	-Quantity and characteristics of aqueous and solid residuals generated by system operation
Cost-Effectiveness	-Capital cost for equipment, engineering, and installation -O&M cost for chemical usage, electricity consumption, and labor

The O&M and operator skill requirements were evaluated based on a combination of quantitative data and qualitative considerations, including the need for pre- and/or post-treatment, level of system automation, extent of preventative maintenance activities, frequency of chemical and/or media handling and inventory, and general knowledge needed for relevant chemical processes and related health and safety practices. The staffing requirements for the system operation were recorded on an Operator Labor Hour Log Sheet.

The quantity of aqueous and solid residuals generated was estimated by tracking the volume of backwash water produced during each backwash cycle. Backwash water was sampled and analyzed for chemical characteristics.

The cost of the system was evaluated based on the capital cost per gal/min (gpm) (or gal/day [gpd]) of design capacity and the O&M cost per 1,000 gal of water treated. This task required tracking the capital cost for equipment, engineering, and installation, as well as the O&M cost for media replacement and disposal, chemical supply, electricity usage, and labor.

### **3.2 System O&M and Cost Data Collection**

The plant operator performed daily, weekly and monthly system O&M and data collection according to instructions provided by the vendor and Battelle. On a daily basis, with the exception of Saturdays and Sundays, the plant operator recorded system operational data, such as pressure, flowrate, volume, and hour meter readings on a Daily System Operation Log Sheet; checked the potassium permanganate (KMnO<sub>4</sub>) tank level; and conducted visual inspections to ensure normal system operations. If any problem occurred, the plant operator contacted the Battelle Study Lead, who determined if the vendor should be contacted for troubleshooting. The plant operator recorded all relevant information, including the problems encountered, corrective actions taken; materials and supplies used, and associated cost and labor required, on a Repair and Maintenance Log Sheet. On a weekly basis, the plant operator measured several water quality parameters on-site, including temperature, pH, dissolved oxygen (DO), and oxidation-reduction potential (ORP), and recorded the data on a Weekly Water Quality Parameters Log Sheet. During the six-month study period, the system was backwashed automatically, except during the monthly backwash sampling events when the system was backwashed manually to capture the required backwash samples. Monthly backwash data also were recorded on a Backwash Log Sheet.

The capital cost for the arsenic removal system consisted of the cost for equipment, site engineering, and system installation. The O&M cost consisted of the cost for chemical usage, electricity consumption, and labor. Consumption of KMnO<sub>4</sub> was tracked on the Daily System Operation Log Sheet. Electricity usage was estimated based on the hours of operation and the chemical feed pump motor size. Labor for various activities, such as routine system O&M, troubleshooting and repairs, and demonstration-related work, were tracked using an Operator Labor Hour Log Sheet. The routine system O&M included activities such as completing field logs, replenishing the KMnO<sub>4</sub> solution, ordering supplies, performing system inspections, and others as recommended by the vendor. The labor for demonstration-related work, including activities such as performing field measurements, collecting and shipping samples, and communicating with the Battelle Study Lead and the vendor, was recorded, but not used for the cost analysis.

### **3.3 Sample Collection Procedures and Schedules**

To evaluate system performance, samples were collected at the wellhead, across the treatment system, during Macrolite<sup>®</sup> filter backwash, and from the distribution system. The sampling schedules and analytes measured during each sampling event are listed in Table 3-3. In addition, Figure 3-1 presents a flow diagram of the treatment system along with the analytes and schedules at each sampling location.

**Table 3-3. Sample Collection Schedule and Analyses**

Sample Type	Sample Locations <sup>(a)</sup>	No. of Samples	Frequency	Analytes	Date(s) Samples Collected
Source Water	At Wellhead (IN)	1	Once (during initial site visit)	On-site: pH, temperature, DO, and ORP Off-site: As(III), As(V), As (total and soluble), Fe (total and soluble), Mn (total and soluble), U (total and soluble), V (total and soluble), Na, Ca, Mg, Cl, F, NO <sub>3</sub> , NO <sub>2</sub> , NH <sub>3</sub> , SO <sub>4</sub> , SiO <sub>2</sub> , P, turbidity, alkalinity, TDS, and TOC	08/31/04
Treatment Plant Water	At Wellhead (IN), After Contact Tanks (AC), After Tanks A/B (TA/TB), After Tank C/D (TC/TD)	4	Weekly	On-site: pH, temperature, DO, and ORP Off-site: As(total), Fe(total), Mn(total), SiO <sub>2</sub> , P, turbidity, and alkalinity	07/20/05, 07/26/05, 08/02/05, 08/24/05, 08/31/05, 09/07/05, 09/14/05, 09/27/05, 10/05/05, 10/12/05, 10/26/05, 11/02/05, 11/09/05, 11/29/05, 12/14/05, 01/10/06, 01/17/06
	At Wellhead (IN), After Contact Tanks (AC), After Tanks TA/TB and TC/TD Combined (TT)	3	Monthly	Same as weekly analytes shown above plus the following: Off-site: As (soluble), As(III), As(V), Fe (soluble), Mn (soluble), Ca, Mg, F, NO <sub>3</sub> , SO <sub>4</sub> , and TOC	07/13/05, 08/18/05, 09/20/05, 10/19/05, 11/15/05, 12/08/05, 01/05/06
Distribution Water	Three LCR Residences	3	Monthly	As (total), Fe (total), Mn (total), Cu, Pb, pH, and alkalinity	Baseline Sampling <sup>(b)</sup> 02/16/05, 03/23/05 04/19/05, 05/23/05 Monthly Sampling: 07/26/05, 09/07/05, 09/27/05, 11/02/05, 11/29/05, 12/15/05, 01/17/06
Backwash Water	Backwash Discharge Line	2	Monthly	As (total and soluble), Fe (total and soluble), Mn (total and soluble), pH, turbidity, TDS, and TSS	09/08/05, 09/20/05, 10/12/05, 11/15/05, 12/08/05, 01/10/06
Residual Sludge	At Backwash Discharge Point	2-3	TBD	TCLP Metals	TBD

(a) Abbreviation corresponding to sample location in Figure 3-1.

(b) Sampling events performed before system startup.

TBD = to be determined.

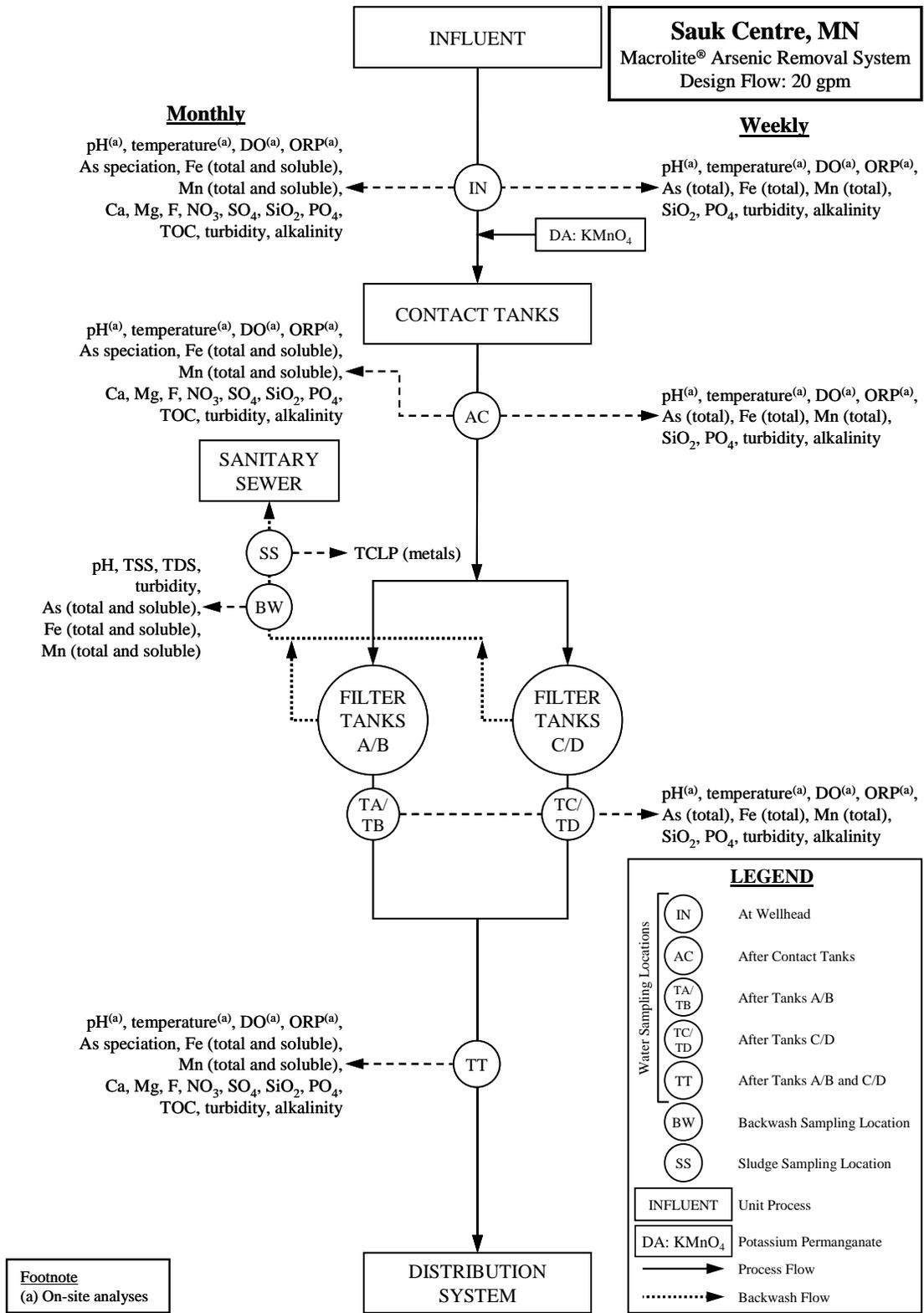


Figure 3-1. Process Flow Diagram and Sampling Locations

Specific sampling requirements for analytical methods, sample volumes, containers, preservation, and holding times are presented in Table 4-1 of the EPA- Quality Assurance Project Plan (QAPP) (Battelle, 2004). The procedure for arsenic speciation is described in Appendix A of the QAPP.

**3.3.1 Source Water.** During the initial visit to the site, one set of source water samples was collected and speciated using an arsenic speciation kit (see Section 3.4.1). The sample tap was flushed for several minutes before sampling; special care was taken to avoid agitation, which might cause unwanted oxidation. Analytes for the source water samples are listed in Table 3-3.

**3.3.2 Treatment Plant Water.** During the system performance evaluation study, the plant operator collected samples weekly, on a four-week cycle, for on- and off-site analyses. For the first week of each four-week cycle, samples taken at the wellhead (IN), after the contact tanks (AC), and after Tanks A/B and Tanks C/D combined (TT), were speciated on-site and analyzed for the analytes listed in Table 3-3 for monthly treatment plant water. For the next three weeks, samples were collected at IN, AC, after Tanks A/B (TA/TB) and after Tanks C/D (TC/TD) and analyzed for the analytes listed in Table 3-3 for the weekly treatment plant water.

**3.3.3 Special Study - KMnO<sub>4</sub> Jar Tests.** Because significantly elevated soluble manganese concentrations were measured in the treated water after the Macrolite<sup>®</sup> filters, a series of jar tests were conducted at Battelle’s laboratories on November 7, 2005, using the treated water taken at the TT location from the site to determine an appropriate KMnO<sub>4</sub> dosage for complete oxidation of Mn(II) and formation of filterable manganese solids.

The jar tests consisted of six 1-L jars of the treated water with increasing dosages of KMnO<sub>4</sub> ranging from 1.0 to 3.0 mg/L (Table 3-4). One jar was used as a control with no KMnO<sub>4</sub> addition. The jars were placed on a Phipps & Byrd overhead stirrer/jar tester with an illuminated base. The jars were mixed for a total of 31 min at various mixing speeds: 200 rpm for 1 min immediately after the KMnO<sub>4</sub> addition, followed by 100 rpm for 19 min and 28 rpm for 11 min. After the specified contact time, the supernatant in each jar was filtered with 0.20-µm disc filters and analyzed for arsenic, iron, and manganese using Inductively Coupled Plasma-Mass Spectrometry (ICP-MS). The pH and ORP values of the content in each jar also were measured using a VWR Symphony SP90M5 Handheld Multimeter at the beginning and end of each jar test. The results of the jar tests are discussed in Section 4.5.1.

**Table 3-4. Summary of Jar Test Parameters**

Parameter	Jar 1	Jar 2	Jar 3	Jar 4	Jar 5	Jar 6
Mix Time (min) <sup>(a)</sup>	31	31	31	31	31	31
KMnO <sub>4</sub> (mg/L)	0	1.0	1.5	2.0	2.5	3.0

(a) Mixing Speeds: 1 min at 200 rpm, 19 min at 100 rpm, and 11 min at 28 rpm.

**3.3.4 Backwash Water.** Backwash samples were collected monthly by the plant operator. One backwash water sample was collected as one of the tanks in each duplex unit was backwashed during each of the first six monthly sampling events. For the first three sampling events, one grab sample was taken as the bulk of solids/water mixture was being discharged from the sample tap located on the backwash water discharge line but before the backwash totalizer. Unfiltered samples sent to American Analytical Laboratories (AAL) for pH, total dissolved solids (TDS), and turbidity measurements. Filtered samples using 0.45-µm disc filters were sent to Battelle’s ICP-MS laboratory for soluble As, Fe, and Mn analyses. Starting from November 15, 2005, during the fourth sampling event, the sampling procedure

was modified to include the collection of composite samples for total As, Fe, and Mn as well as TSS analyses. This modified procedure involved diverting a portion of backwash water at approximately 1 gpm into a clean, 32-gal plastic container over the duration of the backwash for each set of duplex tanks. After the content in the container was thoroughly mixed, composite samples were collected and /or filtered on-site with a 0.45- $\mu$ m filters. Analytes for the backwash samples are listed in Table 3-3.

**3.3.5 Residual Solids.** Residual solids produced by the treatment process included backwash solids, which were not collected during the initial six months of this demonstration.

**3.3.6 Distribution System Water.** Samples were collected from the distribution system to determine the impact of the arsenic treatment system on the water chemistry in the distribution system, specifically, the arsenic, lead, and copper levels. Prior to the system startup, from February to May 2005, four sets of baseline distribution water samples were collected from three residences within the distribution system. Following the system startup, distribution system sampling continued on a monthly basis at the same three locations.

The three homes selected for the sampling had been included in the Park's Lead and Copper Rule (LCR) sampling. The homeowners collected samples following an instruction sheet developed according to the *Lead and Copper Monitoring and Reporting Guidance for Public Water Systems* (EPA, 2002). First draw samples were collected from a cold-water faucet located upstream of the softener in each home. (Note that the samples thus collected were not from a frequently used kitchen or bathroom faucet nor from a faucet that was commonly used for human consumption.) To ensure collection of stagnant water, the faucet were not used for at least 6 hr. Dates and times of sample collection and last water usage were recorded for calculations of the stagnation time. Analytes for the distribution system water are listed in Table 3-3. Arsenic speciation was not performed for the distribution water samples.

## **3.4 Sampling Logistics**

**3.4.1 Preparation of Arsenic Speciation Kits.** The arsenic field speciation method uses an anion exchange resin column to separate the soluble arsenic species, As(V) and As(III) (Edwards et al., 1998). Resin columns were prepared in batches at Battelle laboratories according to the procedures detailed in Appendix A of the EPA-endorsed QAPP (Battelle, 2004).

**3.4.2 Preparation of Sample Coolers.** For each sampling event, a sample cooler was prepared with the appropriate number and type of sample bottles, disc filters, and/or speciation kits. All sample bottles were new and contained appropriate preservatives. Each sample bottle was affixed with a pre-printed, colored-coded label consisting of the sample identification (ID), date and time of sample collection, collector's name, site location, sample destination, analysis required, and preservative. The sample ID consisted of a two-letter code for a specific water facility, sampling date, a two-letter code for a specific sampling location, and a one-letter code designating the arsenic speciation bottle (if necessary). The sampling locations at the treatment plant were color-coded for easy identification. The labeled bottles for each sampling locations were placed in separate Ziplock<sup>TM</sup> bags and packed in the cooler.

In addition, all sampling-and shipping-related materials, such as disposable gloves, sampling instructions, chain-of-custody forms, prepaid/addressed FedEx air bills, and bubble wrap, was included. The chain-of-custody forms and air bills were complete except for the operator's signature and the sample dates and times. After preparation, the sample cooler was sent to the site via FedEx for the following week's sampling event.

**3.4.3 Sample Shipping and Handling.** After sample collection, samples for off-site analyses were packed carefully in the original coolers with wet ice and shipped to Battelle. Upon receipt, the sample

custodian verified that all samples indicated on the chain-of-custody forms were included and intact. Sample IDs were checked against the chain-of-custody forms and the samples were logged into the laboratory sample receipt log. Discrepancies noted by the sample custodian were addressed with the plant operator by the Battelle Study Lead.

Samples for metal analyses were stored at Battelle's ICP-MS Laboratory. Samples for other water quality analyses were packed in separate coolers and picked up by couriers from American Analytical Laboratories (AAL) in Columbus, OH and TCCI Laboratories (TCCI) in Lexington, OH, both of which were under contract with Battelle for this demonstration study. The chain-of-custody forms remained with the samples from the time of preparation through analysis and final disposition. All samples were archived by the appropriate laboratories for the respective duration of the required hold time and disposed of properly thereafter.

### **3.5 Analytical Procedures**

The analytical procedures described in detail in Section 4.0 of the EPA-endorsed QAPP (Battelle, 2004) were followed by Battelle ICP-MS, AAL, and TCCI Laboratories. Laboratory quality assurance/quality control (QA/QC) of all methods followed the prescribed guidelines. Data quality in terms of precision, accuracy, method detection limits (MDL), and completeness met the criteria established in the QAPP (i.e., relative percent difference [RPD] of 20%, percent recovery of 80-120%, and completeness of 80%). The quality assurance (QA) data associated with each analyte will be presented and evaluated in a QA/QC Summary Report to be prepared under separate cover upon completion of the Arsenic Demonstration Project.

Field measurements of pH, temperature, DO, and ORP were conducted by the plant operator using a VWR Symphony SP90M5 Handheld Multimeter, which was calibrated for pH and DO prior to use following the procedures provided in the user's manual. The ORP probe also was checked for accuracy by measuring the ORP of a standard solution and comparing it to the expected value. The plant operator collected a water sample in a clean, plastic beaker and placed the Symphony SP90M5 probe in the beaker until a stable value was obtained. The plant operator also performed free and total chlorine measurements using Hach chlorine test kits following the user's manual.

## 4.0: RESULTS AND DISCUSSION

### 4.1 Facility Description and Pre-Existing Treatment System Infrastructure

Located at 43987 County Road 24 in Sauk Centre, MN, BSLMHP had a water supply system sized for up to 50 mobile home connections or approximately 100 residents. There were 37 mobile homes in the park during the study period. Prior to the demonstration study, the facility reported the average daily demand of 7,500 gpd and the peak daily demand of 16,000 gpd. The system typically operated approximately 6 hr/day. Figure 4-1 shows the pre-existing well house at the facility.

The system was supplied intermittently by groundwater from two wells installed at a depth of approximately 90 ft below ground surface (bgs). The new well (Well No. 2) was used as the primary well and the old well (Well No. 1) used as a backup well. The new well was equipped with a 1½-horsepower (hp), 4-in submersible pump installed on a 60-ft drop pipe and rated for 25 gpm at 180 ft H<sub>2</sub>O (or 78 psi). The pump installed in the backup well reportedly had a similar capacity, but records were no longer available. Figure 4-2 shows the existing piping and two 62-gal Champion pressure tanks in the wellhouse. There was no disinfection or other treatment at the wellheads, although most residents had water softeners in their homes.

**4.1.1 Source Water Quality.** Source water samples were collected on August 31, 2004, and subsequently analyzed for the analytes shown in Table 3-3. The results of source water analyses, along with those provided by the facility to EPA for the demonstration site selection and those independently collected and analyzed by EPA, MDH, and the vendor are presented in Table 4-1.

As shown in Table 4-1, total arsenic concentrations in source water extracted from both wells ranged from 17.0 to 32.0 µg/L. Based on the August 31, 2004, speciation results, as much as 54% of the total arsenic, or 13.6 µg/L, was found to exist as As(III) and 18% existed as particulate arsenic.



**Figure 4-1. Pre-Existing Pump House at BSLMHP, MN Site**



**Figure 4-2. Existing Well Piping and Pressure Tanks at BSLMHP, MN Site**

Iron concentrations in source water extracted from both wells ranged from 3,000 to 3,400  $\mu\text{g/L}$ , existing entirely as soluble iron based on August 31, 2004 results. A rule of thumb is that the soluble iron concentration, expressed in  $\text{mg/L}$ , should be at least 20 times the soluble arsenic concentration, also expressed in  $\text{mg/L}$ , for effective removal of arsenic onto iron solids (Sorg, 2002). Based on the best and worst case scenarios, the results indicate that iron levels are 94 to 200 times higher than total arsenic levels. As such, there is no need to supplement the natural iron for arsenic removal. The proposed treatment process is designed to reduce iron levels in the filtered water to below the secondary MCL of 300  $\mu\text{g/L}$ .

Manganese levels of 130 to 150  $\mu\text{g/L}$  were elevated above the secondary MCL of 50  $\mu\text{g/L}$ . The pH values ranged from 7.1 to 7.4, which were within the target range of 5.5 to 8.5 for the iron removal process. Total organic carbon (TOC) levels at 3.9 to 4.9  $\text{mg/L}$  were high and because of the high levels,  $\text{KMnO}_4$  was used to oxidize iron and arsenic. The use of  $\text{KMnO}_4$  should help eliminate the formation potential of disinfection byproducts, which could occur if pre-chlorination was implemented. In April 2005, EPA conducted a disinfection byproduct formation test on source water and found that after 96 hr of maintaining a chlorine residual, the total trihalomethane (TTHM) level was 0.11  $\text{mg/L}$ , existing almost completely as chloroform. Note that the MCL for TTHM is 0.080  $\text{mg/L}$ . This further confirmed the need to use an alternate oxidant to chlorine. Ammonia levels at 1.2  $\text{mg/L}$  also were elevated and could significantly increase the chlorine demand should chlorine be used as an oxidant. The turbidity of the water at 30 NTU was high, presumably caused by iron precipitation during sample collection and transit. Hardness ranged from 300 to 360  $\text{mg/L}$ , silica from 21 to 25  $\text{mg/L}$ , and sulfate from <4 to 5.4  $\text{mg/L}$ . Based on the historical data provided by MDH, there was no apparent difference in water quality between Wells No. 1 and No. 2. Total arsenic concentrations ranged from 26.0 to 32.0  $\mu\text{g/L}$  for Well No. 1 and from 26.0 to 28.0  $\mu\text{g/L}$  for Well No. 2; total iron concentrations were 3,400 for Well No. 1 and 3,000  $\mu\text{g/L}$  for Well No. 2; and total manganese concentrations were 140  $\mu\text{g/L}$  for Well No. 1 and 130  $\mu\text{g/L}$  for Well No. 2.

**Table 4-1. BSLMHP, MN Water Quality Data**

Parameter	Unit	Facility Well 2 Data	Kinetico Well 2 Data	Battelle Well 2 Data	MDH Well 1 Data	MDH Well 2 Data	MDH Distribution Water Data <sup>(a)</sup>
<i>Date</i>		Not specified	10/14/03	08/31/04	01/25/01 – 08/10/04	01/25/01 – 08/10/04	01/25/01 – 08/10/04
pH	–	7.4	7.3	7.1	7.3	7.4	NS
Temperature	°C	NS	NS	NS	NS	NS	NS
DO	mg/L	NS	NS	1.48	NS	NS	NS
ORP	mV	NS	NS	-98	NS	NS	NS
Total Alkalinity (as CaCO <sub>3</sub> )	mg/L	355	364	363	350	360	NS
Hardness (as CaCO <sub>3</sub> )	mg/L	305	330	360	310	300	340
Turbidity	NTU	NS	NS	30	<1–22	<1–20	<1–22
TDS	mg/L	NS	NS	338	NS	NS	NS
TOC	mg/L	4.9	NS	3.9	NS	4.9	NS
Total N (Nitrite + Nitrate) (as N)	mg/L	NS	NS	NS	NS	NS	<0.05–0.01
Nitrate (as N)	mg/L	NS	NS	<0.04	NS	NS	NS
Nitrite (as N)	mg/L	NS	NS	<0.01	NS	NS	NS
Ammonia (as N)	mg/L	NS	NS	1.2	NS	NS	NS
Chloride	mg/L	1.5	<1.0	<1.0	1.5	1.5	NS
Fluoride	mg/L	NS	0.46	<0.1	NS	NS	0.29
Sulfate	mg/L	5.2	<4.0	<5.0	5.0	5.4	6.6
Silica (as SiO <sub>2</sub> )	mg/L	24	21.4	25	23	24	23.0–24.0
Orthophosphate (as P)	mg/L	0.02	<0.5	<0.1	NS	NS	NS
As (total)	µg/L	26	17	25.3	26.0–32.0	26.0–28.0	18.4–28.0
As (soluble)	µg/L	NS	NS	20.7	NS	NS	NS
As (particulate)	µg/L	NS	NS	4.6	NS	NS	NS
As(III)	µg/L	NS	NS	13.6	NS	NS	NS
As(V)	µg/L	NS	NS	7.1	NS	NS	NS
Fe (total)	µg/L	3,200	3,060	3,078	3,400	3,000	2,900
Fe (soluble)	µg/L	NS	NS	3,149	NS	NS	NS
Mn (total)	µg/L	140	150	150	140	130	140
Mn (soluble)	µg/L	NS	NS	154	NS	NS	NS
U (total)	µg/L	NS	NS	<0.1	NS	NS	NS
U (soluble)	µg/L	NS	NS	<0.1	NS	NS	NS
V (total)	µg/L	NS	NS	0.17	<2	<2	NS
V (soluble)	µg/L	NS	NS	<0.1	NS	NS	NS
Na (total)	mg/L	14	13	17	15	14	13.6
Ca (soluble)	mg/L	72	81	87	72	72	80
Mg (total)	mg/L	30	32	35	31	29	33
Gross-Alpha	pCi/L	NS	NS	NS	NS	NS	<1.00–<1.5
Gross-Beta	pCi/L	NS	NS	NS	NS	NS	<0.40–<0.91
Radon	pCi/L	NS	NS	NS	NS	NS	50–470
Radium-228	pCi/L	NS	NS	NS	NS	NS	<0.59

NS = not sampled.

(a) Samples taken from various residences.

**4.1.2 Distribution System and Treated Water Quality.** Water extracted from both wells blends within the pressure tanks and the distribution system. The park owner indicated that the distribution system is solely constructed of polyvinyl chloride (PVC). Prior to this demonstration project, the treatment system had no disinfection or other treatment at the wellheads, although most residents had water softeners in their homes. The historic arsenic levels detected within the distribution system at

several different sampling points, including residences and the wellhouse distribution entry piping, ranged from 18.4 to 28.0 µg/L based on MDH treated water sampling data shown in Table 4-1.

#### 4.2 Treatment Process Description

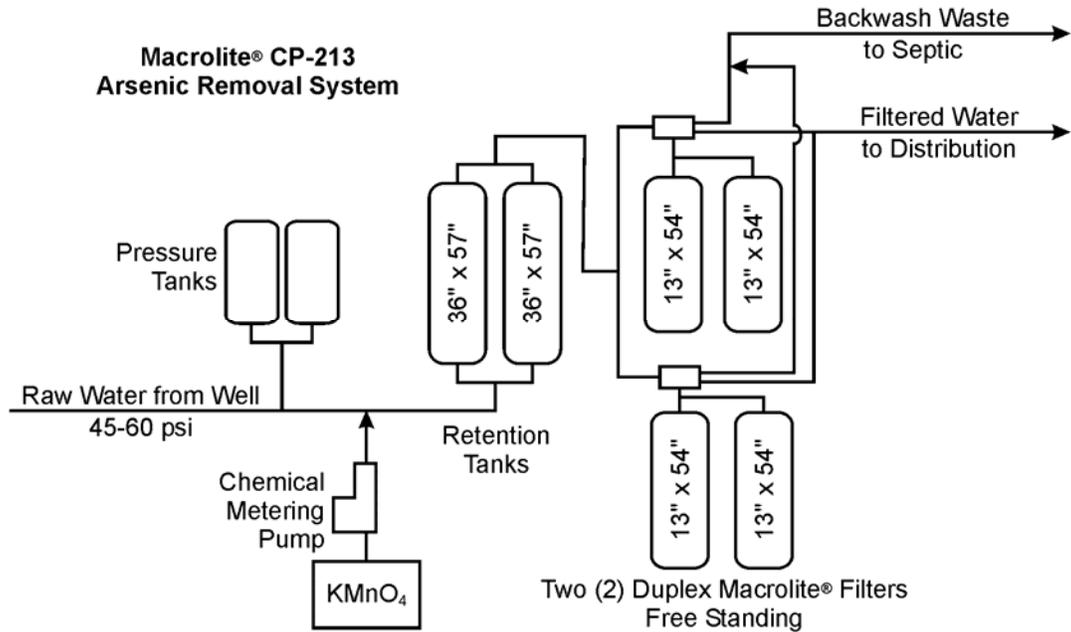
The treatment train for the BSLMHP system includes KMnO<sub>4</sub> oxidation, co-precipitation/adsorption, and Macrolite<sup>®</sup> pressure filtration. Macrolite<sup>®</sup> is an engineered ceramic filtration media manufactured by Kinetico and approved for use in drinking water applications under NSF International (NSF) Standard 61. Macrolite<sup>®</sup> is a low-density, spherical media, designed to allow for filtration rates, as claimed by the vendor, up to 10 gpm/ft<sup>2</sup>, a hydraulic loading rate higher than that for most conventional filtration media. The physical properties of this media are summarized in Table 4-2. The vendor considers Macrolite<sup>®</sup> media chemically inert and compatible with chemicals such as oxidants and ferric chloride.

**Table 4-2. Physical Properties of M2 Macrolite<sup>®</sup> Media**

Property	Value
Color	Variable
Uniformity Coefficient	1.1
Sphere Size Range (mm) [mesh]	0.21 – 0.42 [40 × 70]
Nominal Size (mm)	0.3
Bulk Density (g/cm <sup>3</sup> ) [lb/ft <sup>3</sup> ]	0.86 [54]
Specific Gravity	2.05

Figure 4-3 is a schematic and Figure 4-4 a photograph of the Macrolite<sup>®</sup> CP-213f arsenic removal system. The treatment system was operated as an on-demand system and the volume of water treated was based on water usage. The well pump turned on when the pressure tank pressure reached 45 psi and shut off at 60 psi. The primary system components consisted of a KMnO<sub>4</sub> feed system (with the metering pump interlocked with a totalizer located after the pressure tanks and prior to the treatment system), two contact tanks, four pressure filtration tanks (two each within each duplex unit), and associated pressure and flow instrumentation. Various instruments were installed to track system performance, including the inlet and outlet pressure after each filter, flowrate to the distribution system, and backwash flowrate. All plumbing for the system was Schedule 80 PVC with the necessary valves, sampling ports, and other features. Table 4-3 summarizes the design features of the Macrolite<sup>®</sup> pressure filtration system. The major process steps and system components are presented as follows:

- Potassium Permanganate Oxidation** – KMnO<sub>4</sub> was used to oxidize As(III), Fe(II), and Mn(II) in source water. KMnO<sub>4</sub> was selected to help reduce the formation potential of disinfection by-products due to the presence of high TOC levels in source water. The KMnO<sub>4</sub> addition system consisted of a 150-gal day tank, a Pulsatron metering pump, and an overhead mixer (Figure 4-5). The working solution was prepared by adding 0.75 gal (or 10 lb) of KMnO<sub>4</sub> crystals with 97% minimum purity into 40 gal of water to form a 3% KMnO<sub>4</sub> solution. During the six-month study period, the 21-in diameter and 31.5-in tall KMnO<sub>4</sub> tank was re-filled a total of four times when the tank level reached an average of 17.4 in. The KMnO<sub>4</sub> feed pump was sized with a maximum capacity of 44 gpd or 6.9 L/hr. However, the pump was flow-paced and the actual rate of KMnO<sub>4</sub> addition varied based on the influent



**Figure 4-3. Process Schematic of Macrolite® Pressure Filtration System**



**Figure 4-4. Photograph of Macrolite® Pressure Filtration System**  
 (1. Duplex Units, 2. Contact Tanks, 3. Pressure Tanks,  
 4. Chemical Day Tank, and 5. Totalizer on Raw Water Line)

**Table 4-3. Design Specifications for Macrolite® CP-213f Pressure Filtration System**

Parameter	Value	Remarks
Pretreatment		
KMnO <sub>4</sub> Dosage (mg/L as [KMnO <sub>4</sub> ])	3.3	Calculated KMnO <sub>4</sub> demand based on arsenic, iron, and manganese in source water; actual demand higher due to presence of TOC in source water
Contact Tanks		
Tank Size (in)	36 D × 57 H	205 gal each tank
No. of Tanks	2	–
Configuration	Parallel	–
Contact Time (min/tank)	20	Based on peak flowrate of 20 gpm; actual contact time based on on-demand flowrate
Filtration Tanks		
Tank Size (in)	13 D × 54 H	–
Cross-Sectional Area (ft <sup>2</sup> /tank)	0.92	–
No. of Tanks	4	–
Configuration	Parallel	Between two duplex units and between two filtration tanks within each duplex unit.
Media Type	Macrolite®	40/60 mesh media
Media Quantity (ft <sup>3</sup> /tank)	1.5	20-in bed depth in each tank
Freeboard Measurements (in/tank)	28	Measurements taken by vendor's contractor on 12/07/05 from top of filtration tank to top of media bed
Filtration Rate (gpm/ft <sup>2</sup> )	5.4	Based on a 5 gpm system flowrate through each filtration tank; actual filtration rate based on demand
Pressure Drop (psi)	15	Across a clean bed
Throughput before Backwash (gal)	2,743	Based on initial field design
Backwash Hydraulic Loading Rate (gpm/ft <sup>2</sup> )	6.5	Based on a 6-gpm backwash flowrate through each filtration tank
Backwash Duration (min/tank)	20	–
Wastewater Production (gal)	130	For each tank
System Design Flowrate (gpm)	20	Peak flowrate; actual flowrate based on demand
Maximum Daily Production (gpd)	28,800	Based on peak flowrate, 24 hr/day
Hydraulic Utilization (%)	56	Estimated based on peak daily demand <sup>(a)</sup>

(a) Based on historic peak daily demand of 16,000 gpd.

flowrate to the treatment system. During the first six months of system operation, KMnO<sub>4</sub> dosages varied from 2.1 to 6.1 mg/L. The operator indicated that the mixer was only turned on when the KMnO<sub>4</sub> crystals was mixed initially with water in the day tank.

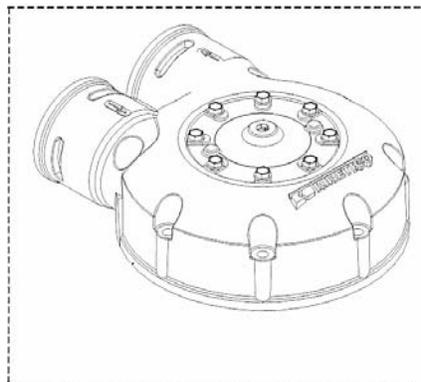
- **Contact** – Two 36-in by 57-in fiberglass reinforced plastic (FRP) contact tanks arranged in parallel provided at least 20 min of contact time when operating at the design (or peak) flowrate of 20 gpm. The longer retention time was designed to aid in the formation of manganese particles before Macrolite® filtration.
- **Pressure Filtration** – The filtration system consisted of downflow filtration through two sets of dual-pressure filtration tanks arranged in parallel. Each duplex unit was comprised of two 13-in by 54-in FRP tanks and a control valve. Each filtration tank was filled with approximately 20-in (1.5 ft<sup>3</sup>) of 40/60 mesh Macrolite® media supported by 3-in (0.25 ft<sup>3</sup>) of garnet underbedding. The standard operation had both tanks of a pair online with each pressure tank treating a maximum of 5 gpm for a hydraulic loading rate



**Figure 4-5. KMnO<sub>4</sub> Feed System**

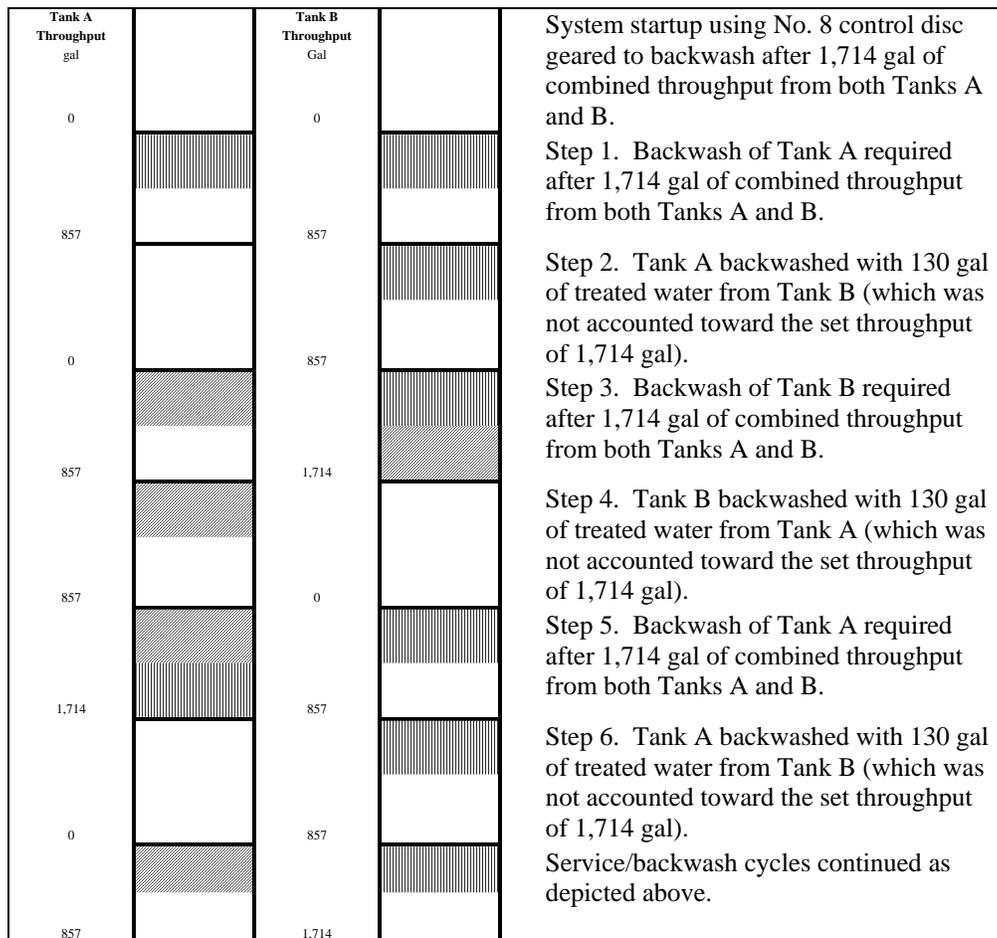
of 5.4 gpm/ft<sup>2</sup>. With four tanks online, the maximum system flowrate was 20 gpm. However, as shown in Figure 4-3, the system had an on-demand configuration with two pressure tanks located ahead of the treatment system. The actual flowrate through the system varied based on water demand, but was limited to less than 20 gpm by flow restrictors located on the duplex units.

The control valve (Kinetico Mach 1250) located on top of each duplex unit (Figure 4-6) consisted of a gear stack, which determines the throughput between two consecutive backwash cycles. The control valve consisted of three chambers: inlet, outlet, and regeneration and only the influent water was measured/recorded by the gear stack.



**Figure 4-6. Kinetico's Mach 1250 Control Valve**

- Backwash Operations** – Backwash was a fully automated process triggered by a pre-set volume throughput measured by the control valve located on top of each duplex unit. The spent filtration tank was backwashed with the treated water from the other tank within the duplex unit and the resulting wastewater was discharged to a sanitary sewer. The backwash duration for each tank was 20 min from start to finish including 15 min of backwash at a flowrate of 6 gpm and a 5 min filter-to-rinse cycle at 6 gpm. The backwash used about 130 gal of the treated water per tank. As discussed in section 4.4.2, it was necessary to increase the frequency of backwash from the initial field setting of every 2,743 gal to every 1,714 gal over the six-month study period. Figure 4-7 depicts the backwash flow paths for one duplex unit (labeled as Tank A and Tank B), which were backwashed on an alternating basis after a pre-set throughput of 1,714 gal. The major steps involved in the backwash process are discussed as follows:



Key

- ||||||| Throughput through Tanks A and B before Tank A Was Backwashed
- ////// Throughput through Tanks A and B before Tank B Was Backwashed
- Clean Bed

**Figure 4-7. Backwash Flow Path for One Duplex Unit with Control Disc No. 8 and a Throughput of 1,714 gal between Backwash Cycles**

Again, both Tank A and Tank B provide the treated water in parallel. The backwash cycles were continuously repeated as shown in Steps 4 through 6 during the treatment system operation. One set of duplex tanks functioned as one unit and always had a filtration capacity between 25% (immediately after backwash of one tank at Step 4) and 75% (right before backwash of the other tank at Step 5).

### 4.3 System Installation

This section provides a summary of system installation activities including permitting, building construction, and system shakedown.

**4.3.1 Permitting.** Engineering plans for the system permit application were prepared by the vendor. The plans included diagrams and specifications for the Macrolite<sup>®</sup> CP-213f arsenic removal system, as well as drawings detailing the connections of the new unit to the pre-existing facility infrastructure. The plans were submitted to MDH on March 28, 2005, and MDH granted its approval of the application on June 14, 2005.

**4.3.2 Building Construction.** The existing well house had an adequate footprint to house the arsenic treatment system. The permit approval issued by MDH on June 14, 2005, indicated a need for an air gap two times the diameter of the filter-to-waste line and a need for all chemicals to be injected on the lower half of the influent pipe. Figure 4-6 shows the chemical injection line located on the top half of the influent pipe. In addition, MDH required the drain line and sewer connection to have at least a 50-ft distance from Well No. 1 and Well No. 2 wellheads and at a lower elevation.

**4.3.3 System Installation, Shakedown, and Startup.** The Macrolite<sup>®</sup> system was shipped on June 10, 2005 and delivered to the site on June 16, 2005. A subcontractor to the vendor off-loaded and installed the system, including piping connections to the existing entry and distribution system. The system installation was completed by June 24, 2005, and the system shakedown was completed by July 3, 2005.

Shakedown activities included disinfection of the contact and filtration tanks and backwash of Macrolite<sup>®</sup> filtration media. The bacteriological test was passed on July 1, 2005. During the startup trip in July, the vendor conducted operator training for system O&M. Battelle arrived on-site on July 13, 2005, to perform system inspections and conduct operator training for system sampling and data collection. The first set of samples for the one year performance evaluation study was taken on July 13, 2005. No major mechanical or installation issues were noted at system startup; however, several pieces of equipment shown in the vendor's June 16, 2005 piping and instrumental diagrams (P&ID) were missing and several installed items did not meet the permit requirements. A list of punch-list items was summarized as follows:

- Install an hour meter.
- Install one raw water sample tap.
- Install one backwash sample tap.
- Install one sample tap after duplex units TA/TB and after duplex units TC/TD.
- Install one pressure gauge after duplex units TA/TB and after duplex units TC/TD.
- Replace the defective pressure gauge beneath the left most pressure tank.
- Install a level sensor on the KMnO<sub>4</sub> day tank.
- Install a ½-inch ball valve on the KMnO<sub>4</sub> injection tube.
- Move the KMnO<sub>4</sub> injection port from the top half of the influent pipe to the lower half per permit requirements.

- Verify that the air gap was two times the filter-to-waste pipe between the drain and the filter-to-waste pipe.

All punch-list items were resolved by the vendor by September 30, 2005.

#### 4.4 System Operation

**4.4.1 Operational Parameters.** Table 4-4 summarizes the operational parameters for the first six months of system operation, including operational time, throughput, flowrate, and pressure. Detailed daily operational information also is provided in Appendix A.

Between July 13, 2005, and January 17, 2006, the primary well pump operated for approximately 617 hr, with an average daily operating time of 3.4 hr/day (compared to 6 hr/day provided by the park owner prior to the demonstration study) based on the readings of an hour meter installed on the primary well on September 28, 2005. Prior to this time period, the operational time was estimated based on the wellhead totalizer readings and an average well pump flowrate of 25 gpm. The total system throughput during the first six months was approximately 863,470 gal based on the totalizer before entering the distribution system. The average daily demand was 4,617 gal (vs. 7,500 gal provided by the park owner) and the peak daily demand occurred on July 21, 2005, at 14,300 gal (compared to 16,000 gpd provided by the park owner).

The flowrates through the CP-213f system varied due to the on-demand system configuration. Withdrawn from the two pressure tanks located upstream of the system, the on-demand flowrates ranged from 1 to 15 gpm and averaged 4.4 gpm, corresponding to a contact time of 27 to 410 min compared to a design value of 20 min. At these flowrates, the hydraulic loading rates to the filter ranged from 0.3 to 4.1 gpm/ft<sup>2</sup> compared to the design value of 5.4 gpm/ft<sup>2</sup>. Note that Macrolite<sup>®</sup> filter media is rated for a maximum hydraulic loading rate of 10 gpm/ft<sup>2</sup>.

At flowrates of 1 to 15 gpm, the inlet pressure to the system ranged from 40 to 60 psi (compared to the pressure tank set points from 45 to 60 psi) and the outlet pressure ranged from 22 to 55 psi. The total pressure differential ( $\Delta P$ ) readings across the system ranged from 0 to 25 psi depending on the flowrates. The  $\Delta P$  across Tanks A and B ranged from 0 to 25 psi and across Tanks C and D from 2 to 16 psi based on inlet and outlet pressure gauge readings.

During this time period, a total number of 431 backwash cycles took place. The throughput values between two consecutive backwash cycles ranged from 1,714 to 6,857 gal depending on the settings of the control disc located on top of each set of duplex units. The backwash frequency ranged from 0 to 5 tanks backwashed per day. There was one outlier on August 9, 2005, when over 1,720 gal of backwash water was produced (equivalent to 13 backwash events in a single day). The vendor's contractor determined that sediment was lodged in the purge/control valve on one of the duplex units, preventing the valve from being closed; therefore, the duplex unit was stuck in the backwash mode before the operator bypassed the system.

**4.4.2 Backwash.** The backwash was initiated by throughput. The control disc located on top of each duplex unit determined the throughput before backwash. Table 4-5 summarizes the backwash frequency based on four control disc sizes installed over the six-month study period. The vendor switched out the control discs four times (although one was done in error) due to observations of particulate arsenic, iron, and manganese breakthrough through the Macrolite<sup>®</sup> filters. Control disc No. 5 geared to backwash after a throughput of 2,743 gal was used from system startup on July 13, 2005, through September 20, 2005. The actual throughput values between two consecutive backwash cycles averaged 2,449 gal based on the total volume of water treated and the total number of tanks

**Table 4-4. System Operation from July 13, 2005 to January 17, 2006**

<b>Parameter</b>	<b>Values</b>
<b><i>Primary Well Pump (Well No. 2)</i></b>	
Total Operating Time (hr)	617.3 <sup>(a)</sup>
Average Daily Operating Time (hr)	3.4 <sup>(a)</sup>
Range of Flowrates (gpm)	23–31 <sup>(b)</sup>
Average Flowrate (gpm)	25 <sup>(b)</sup>
<b><i>System Throughput/Demand</i></b>	
Throughput to Distribution (gal)	863,470
Average Daily Demand (gpd)	4,617
Peak Daily Demand (gpd)	14,300
<b><i>CP-213f System – Service Mode</i></b>	
Range of Flowrates (gpm)	1–15 <sup>(c)</sup>
Average Flowrate (gpm)	4.4 <sup>(c)</sup>
Range of Contact Times (min)	27–410
Average Contact Time (min)	114
Range of Hydraulic Loading Rates to Filters (gpm/ft <sup>2</sup> )	0.3–4.1
Average Hydraulic Loading Rate to Filters (gpm/ft <sup>2</sup> )	2.2
Range of System Inlet Pressure (psi)	40–60
Range of System Outlet Pressure (psi)	22–55
Range of $\Delta p$ Readings across System (psi)	0–25
<b><i>CP-213 System – Backwash Mode</i></b>	
Number of Backwash Cycles	431 <sup>(d)</sup>
Throughput between Backwash Cycles (gal)	1,714–6,857 <sup>(e)</sup>
Number of Backwash Cycles Per Day	0–5

- (a) Hour meter installed on September 28, 2005. Run time before this period estimated based on wellhead totalizer readings and average well flowrate of 25 gpm.
- (b) Based on totalizer on raw water line and hour meter readings; excluding data from September 29, October 5, and October 6, 2005.
- (c) Based on flow meter readings located on treated water line recorded starting September 28, 2005.
- (d) Based on totalizer readings on backwash water discharge line and 130 gal of wastewater produced during backwash of each tank.
- (e) Backwash triggered by volume of water treated based on settings of control discs located on top of each set of duplex filtration tanks.

backwashed. The number of tanks backwashed per day ranged from 0 to 5 except for the outlier on August 9, 2005, discussed in Section 4.4.1. Because breakthrough of particulate arsenic, iron, and manganese was observed, the vendor dispatched its contractor to the site to install a new control disc in an attempt to curb the particulate breakthrough. While a higher number disc should have been used, a disc with a lower number (i.e., No. 2 geared to backwash after a throughput of 6,857 gal) was inadvertently installed by the contractor between September 21 through 29, 2005. On September 30, 2005, No. 2 disc was replaced with a No. 7 disc, which was geared for a throughput of 1,957 gal. The average throughput for the No. 7 disc was 1,932 gal and the number of tanks backwashed per day ranged from 0 to 5. For this reason, control disc No. 8 was subsequently installed on December 7, 2005 to further reduce the throughput to 1,714 gal. The actual throughput was 1,684 gal and the number of tanks backwashed per day ranged from 1 to 5.

**Table 4-5. Control Disc Size and Throughput between Backwash Cycles**

<b>Duration</b>	<b>Control Disc</b>	<b>Design Throughput between Consecutive Backwash Cycles (gal)</b>	<b>Average Throughput between Consecutive Backwash Cycles (gal)</b>	<b>Number of Tanks Backwashed (No./day)</b>	<b>Backwash Water Generation Ratio (%)</b>
07/13/05-09/20/05	No. 5	2,743	2,449	0-5	5.5
09/21/05-09/29/05	No. 2	6,857	3,469	0-3	2.8
09/30/05-12/06/05	No. 7	1,957	1,932	0-5	6.6
12/07/05-01/17/06	No. 8	1,714	1,684	1-5	7.2

However, after the disc No. 8 changeout, particulate breakthrough continued to be observed. Except for disc No. 2, the ratios of backwash water generated ranged from 5.5% to 7.2% and averaged 6.4%.

**4.4.3 Residual Management.** Residuals produced by the operation of the Macrolite<sup>®</sup> system included backwash water and associated solids, which were discharged to a nearby septic system for disposal.

**4.4.4 System/Operation Reliability and Simplicity.** During the first six months of system operation, several instances of total arsenic and iron breakthrough were observed in service mode and the backwash frequency had to be increased twice by switching out the control valve on top of each set of duplex units. The required system O&M and operator skill levels are discussed according to pre- and post-treatment requirements, levels of system automation, operator skill requirements, preventive maintenance activities, and frequency of chemical/media handling and inventory requirements.

**Pre- and Post-Treatment Requirements.** Pre-treatment included KMnO<sub>4</sub> addition for the oxidation of arsenic and iron. Specific chemical handling requirements are further discussed below under chemical handling and inventory requirements. KMnO<sub>4</sub> was selected as an alternative oxidant due to the high TOC levels in source water and the potential to form disinfection byproducts should chlorine be used as an oxidant. However, as discussed in Section 4.5.1, it was determined that source water had a relatively elevated KMnO<sub>4</sub> demand, which resulted in some difficulty in controlling the effluent manganese levels (both particulate and soluble forms) and ensuring that the MnO<sub>4</sub><sup>-</sup> added was completely reduced to form MnO<sub>2</sub> solids.

**System Automation.** All major functions of the treatment system were automated and would require only minimal operator oversight and intervention if all functions were operating as intended. Automated processes included system startup in service mode when the well energized, backwash cycling based on throughput, fast rinse cycling, and system shutdown when the well pump shut down. However, as noted in Section 4.4.1, an operational issue did arise with the automated system backwash on August 9, 2005. Due to the small size of the arsenic treatment system, the operational data was collected manually by the operator mentioned in the next paragraph.

**Operator Skill Requirements.** Under normal operating conditions, the skill set required to operate the Macrolite<sup>®</sup> system was limited to observation of the process equipment integrity and operating parameters such as pressure and flow. The daily demand on the operator was about 5 min to visually inspect the system and record operating parameters on the log sheets. Other skills needed including performing O&M activities such as replenishing the KMnO<sub>4</sub> solution in the chemical drum, monitoring backwash operational issues, and working with the vendor to troubleshoot and perform minor on-site repairs.

For the state of Minnesota, there are five water operator certificate class levels, i.e., A, B, C, D, and E, with Class A being highest. The certificate levels are based on education, experience, and system characteristics, such as water source, treatment processes, water storage volume, number of wells, and population affected. The operator for the BSLMHP system has a Class D certificate. Class D requires a high school diploma or equivalent with at least one year of experience in operating a Class A, B, C, or D system or a postsecondary degree from an accredited institution.

**Preventive Maintenance Activities.** Preventive maintenance tasks recommended by the vendor included daily to monthly visual inspection of the piping, valves, tanks, flow meters, and other system components. The pump on the primary well (Well No. 2) developed a leak and had to be shut down temporarily on January 4, 2006 for repairs. Meanwhile, Well No. 1 was turned on as the backup well. The leak on the Well No. 2 pump was repaired the next day and the primary well resumed its normal operation thereafter..

**Chemical/Media Handling and Inventory Requirements.**  $\text{KMnO}_4$  addition was implemented since the system startup on July 13, 2005. The mixing of the  $\text{KMnO}_4$  solution required only 10 min to complete, as reported by the operator. The chemical consumption was checked each day as part of the routine operational data collection. Several adjustments were made over time to optimize the  $\text{KMnO}_4$  dosage for the oxidation of arsenic, iron, and manganese.

#### 4.5 System Performance

The performance of the Macrolite<sup>®</sup> CP-213f arsenic removal system was evaluated based on analyses of water samples collected from the treatment plant, backwash lines, and distribution system.

**4.5.1 Treatment Plant Sampling.** Water samples were collected at five locations across the treatment train: at the wellhead (IN), after the contact tanks (AC), after the first set of duplex unit tanks A and B (TA/TB), after the second set of duplex tanks C and D (TC/TD), and after the two sets of duplex tanks combined (TT). Sampling was conducted on 26 occasions (including two duplicate sampling events) during the first six months of system operation, with field speciation performed on samples collected from the IN, AC, and TT locations for 7 of the 26 occasions. Table 4-6 summarizes the arsenic, iron, and manganese analytical results. Table 4-7 summarizes the results of the other water quality parameters. Appendix B contains a complete set of analytical results through the first six months of system operation. The results of the water treatment plant samples with the addition of a varying amount of  $\text{KMnO}_4$  before and after the November 7, 2005, manganese jar tests are discussed below.

**Arsenic and Iron Removal.** Total arsenic concentrations in raw water ranged from 20.6 to 36.6  $\mu\text{g/L}$  and averaged 27.7  $\mu\text{g/L}$ . As(III) was the predominant species with concentrations ranging from 13.9 to 27.4  $\mu\text{g/L}$  and averaging 23.0  $\mu\text{g/L}$  (Table 4-6 and Figure 4-8). Only trace amounts of particulate As and As(V) existed in raw water, with concentrations averaging 2.1 and 4.0  $\mu\text{g/L}$ , respectively. The total arsenic concentrations measured during this six-month period were consistent with those of the historical source water sampling (Table 4-1), although the As(III) concentrations were significantly higher, representing over 83% of the total concentrations in source water (compared to 54% during the August 31, 2004, source water sampling). The existence of As(III) as the predominating arsenic species was consistent with the low DO concentrations (averaged 1.2 mg/L, Table 4-7) and low ORP values (ranged from -76 to -23 mV and averaged -46 mV) in source water.

As shown in Table 4-6, total iron concentrations in raw water ranged from 1,069 to 3,758  $\mu\text{g/L}$  and averaged 2,760  $\mu\text{g/L}$ . Iron in raw water existed almost entirely in the soluble form with an average value of 2,691  $\mu\text{g/L}$ . The presence of predominating soluble iron also was consistent with the presence of

**Table 4-6. Summary of Arsenic, Iron, and Manganese Analytical Results**

Parameter	Sampling Location	Sample Count	Concentration (µg/L)			Standard Deviation
			Minimum	Maximum	Average	
As (total)	IN	26	20.6	36.6	27.7	4.0
	AC	26	5.6	36.1	26.3	5.5
	TA/TB	17	2.0	29.8	8.8	7.5
	TC/TD	17	2.1	17.5	7.3	4.4
	TT	9	2.9	17.7	7.6	5.7
As (soluble)	IN	7	24.4	30.3	27.0	2.1
	AC	7	2.7	8.7	4.4	2.1
	TT	7 <sup>(a)</sup>	2.0	6.2	3.5	1.5
As (particulate)	IN	7	0.1	6.1	2.1	2.6
	AC	7	18.4	26.3	22.9	2.6
	TT	7 <sup>(a)</sup>	0.1	10.9	2.2	3.9
As(III)	IN	7	13.9	27.4	23.0	4.5
	AC	7	0.3	5.4	1.9	1.8
	TT	7 <sup>(a)</sup>	0.4	4.4	1.8	1.5
As(V)	IN	7	<0.1	16.5	4.0	5.7
	AC	7	1.7	3.3	2.6	0.6
	TT	7 <sup>(a)</sup>	1.3	2.4	1.7	0.3
Fe (total)	IN	26	1,069	3,758	2,760	441
	AC	26	247	3,173	2,598	521
	TA/TB	17	12	2,363	394	635
	TC/TD	17	<25	1,140	259	364
	TT	9	<25	1,067	308	361
Fe (soluble)	IN	7	2,263	2,954	2,691	255
	AC	7	<25	306	56.3	110
	TT	7 <sup>(a)</sup>	<25	40.7	<25	<25
Mn (total)	IN	26	110	430	144	59.7
	AC	26	416	1,506	955	235
	TA/TB	17	203	1,002	648	254
	TC/TD	17	187	971	650	257
	TT	9	331	1,091	644	256
Mn (soluble)	IN	7	110	145	132	12.2
	AC	7	108	946	492	317
	TT	7 <sup>(a)</sup>	138	1,062	565	363

One-half of detection limit used for non-detect samples for calculations.

Duplicate samples included calculations.

(a) On December 28, 2005, arsenic speciation results taken at IN, AC, TA/TB, and TC/TD locations. Average concentration used for TT location.

predominating As(III) as well as low DO concentrations and low ORP values. Given the average soluble iron and soluble arsenic levels in source water, this corresponded to an iron:arsenic ratio of 100:1, which was well above the target ratio of 20:1 for effective removal of arsenic (Sorg, 2002).

After KMnO<sub>4</sub> addition and the contact tanks, As(III) concentrations ranged from 0.3 to 5.4 µg/L and averaged 1.9 µg/L (Table 4-6 and Figure 4-8), suggesting effective oxidation of As(III) to As(V) with KMnO<sub>4</sub>. Particulate arsenic concentrations after the contact tanks ranged from 18.4 to 26.3 µg/L and averaged 22.9 µg/L, representing most of the total arsenic (averaged 26.3 µg/L) after the contact tanks. After KMnO<sub>4</sub> addition and the contact tanks, total iron concentrations averaged 2,598 µg/L, existing almost entirely in particulate form. This data suggested effective oxidation of arsenic and iron even in the

**Table 4-7. Summary of Other Water Quality Parameter Sampling Results**

Parameter	Sampling Location	Unit	Sample Count	Concentration/Unit			Standard Deviation
				Minimum	Maximum	Average	
Alkalinity (as CaCO <sub>3</sub> )	IN	mg/L	26	352	383	366	11
	AC	mg/L	26	321	383	368	11
	TA/TB	mg/L	17	352	378	369	8
	TC/TD	mg/L	17	352	383	369	9
	TT	mg/L	9	361	383	371	7
Fluoride	IN	mg/L	7	0.2	0.2	0.2	0
	AC	mg/L	7	0.2	0.2	0.2	0
	TT	mg/L	7 <sup>(a)</sup>	0.2	0.2	0.2	0
Sulfate	IN	mg/L	7	<1	<1	<1	0
	AC	mg/L	7	<1	<1	<1	0
	TT	mg/L	7 <sup>(a)</sup>	<1	<1	<1	0
Nitrate (as N)	IN	mg/L	7	<0.05	0.06	0.03	0
	AC	mg/L	7	<0.05	0.06	0.03	0
	TT	mg/L	7 <sup>(a)</sup>	<0.05	0.25	0.06	0.1
Orthophosphate (as P)	IN	mg/L	12	<0.05	<0.05	<0.05	0
	AC	mg/L	12	<0.05	<0.05	<0.05	0
	TA/TB	mg/L	6	<0.05	<0.05	<0.05	0
	TC/TD	mg/L	6	<0.05	<0.05	<0.05	0
	TT	mg/L	6	<0.05	<0.05	<0.05	0
P (total) (as P)	IN	mg/L	15	0.4	0.6	0.5	0.04
	AC	mg/L	15	0.1	0.5	0.4	0.1
	TA/TB	mg/L	12	<0.03	0.4	0.1	0.1
	TC/TD	mg/L	12	<0.03	0.2	0.1	0.1
	TT	mg/L	3	0.1	0.2	0.1	0.1
Silica (as SiO <sub>2</sub> )	IN	mg/L	26	22.6	29.4	24.3	1.4
	AC	mg/L	26	22.5	28.6	24.4	1.3
	TA/TB	mg/L	17	22.5	28.4	24.4	1.4
	TC/TD	mg/L	17	22.7	28.2	24.6	1.3
	TT	mg/L	9	21.7	24.7	23.4	1.0
Turbidity	IN	NTU	26	13.0	35.0	30.0	5.0
	AC	NTU	26	2.8	6.5	4.0	1.1
	TA/TB	NTU	17	<0.1	14.0	1.5	3.4
	TC/TD	NTU	17	<0.1	14.0	2.0	3.4
	TT	NTU	9	0.1	11.0	1.9	3.5
TOC	IN	mg/L	4	3.2	4.8	4.0	0.7
	AC	mg/L	4	3.1	4.6	3.7	0.7
	TT	mg/L	4	3.0	4.8	3.9	0.7
pH	IN	S.U.	23	7.2	7.5	7.3	0.1
	AC	S.U.	23	7.2	7.6	7.4	0.1
	TA/TB	S.U.	14	7.2	7.4	7.3	0.1
	TC/TD	S.U.	14	7.2	7.5	7.4	0.1
	TT	S.U.	9	7.2	7.7	7.3	0.2
Temperature	IN	°C	23	9.3	14.9	10.7	1.4
	AC	°C	23	9.4	14.1	10.9	1.5
	TA/TB	°C	14	9.3	12.5	10.2	0.8
	TC/TD	°C	14	9.2	12.8	10.3	0.9
	TT	°C	9	9.5	13.8	11.6	1.5

**Table 4-7. Summary of Other Water Quality Parameter Sampling Results (Continued)**

Parameter	Sampling Location	Unit	Sample Count	Concentration/Unit			Standard Deviation
				Minimum	Maximum	Average	
DO	IN	mg/L	23	0.7	3.6	1.2	0.7
	AC	mg/L	23	0.5	3.1	1.1	0.5
	TA/TB	mg/L	14	0.5	1.6	0.9	0.3
	TC/TD	mg/L	14	0.5	1.3	0.9	0.2
	TT	mg/L	9	0.7	1.2	0.9	0.2
ORP	IN	mV	23	-76	-23	-46	14
	AC	mV	23	-22	196	62	56
	TA/TB	mV	14	-9	177	67	51
	TC/TD	mV	14	-12	183	72	55
	TT	mV	9	5.8	219	106	78
Total Hardness (as CaCO <sub>3</sub> )	IN	mg/L	7	296	383	319	28.8
	AC	mg/L	7	295	330	315	10.9
	TT	mg/L	7 <sup>(a)</sup>	305	338	319	12.0
Ca Hardness (as CaCO <sub>3</sub> )	IN	mg/L	7	177	228	191	16.6
	AC	mg/L	7	178	197	189	6.8
	TT	mg/L	7 <sup>(a)</sup>	176	212	191	11.5
Mg Hardness (as CaCO <sub>3</sub> )	IN	mg/L	7	112	155	128	14.0
	AC	mg/L	7	114	133	126	6.4
	TT	mg/L	7 <sup>(a)</sup>	120	136	128	5.3

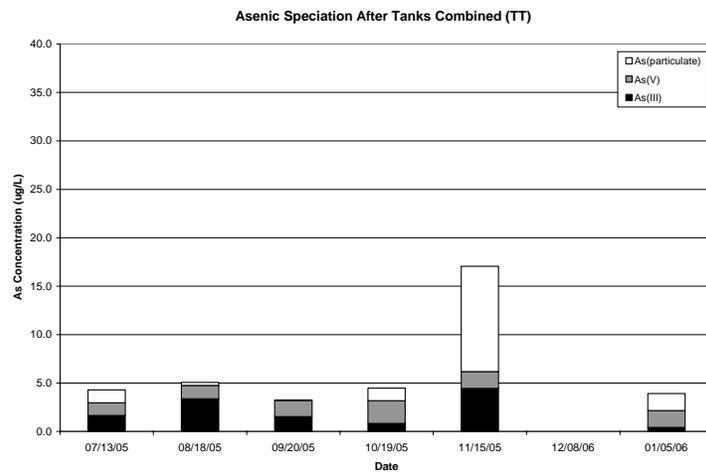
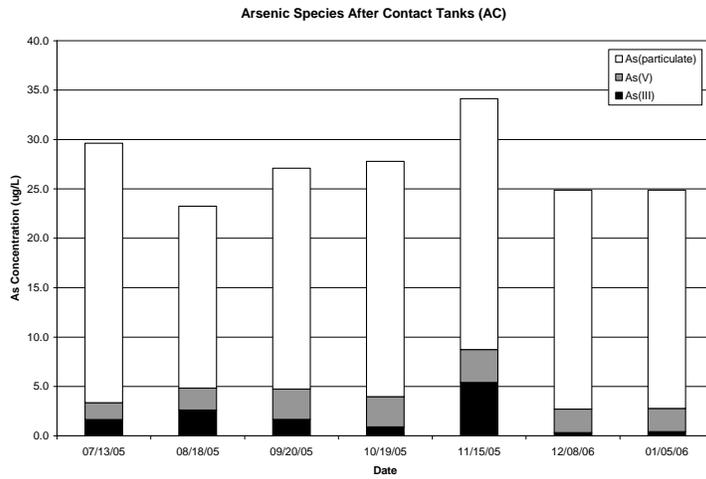
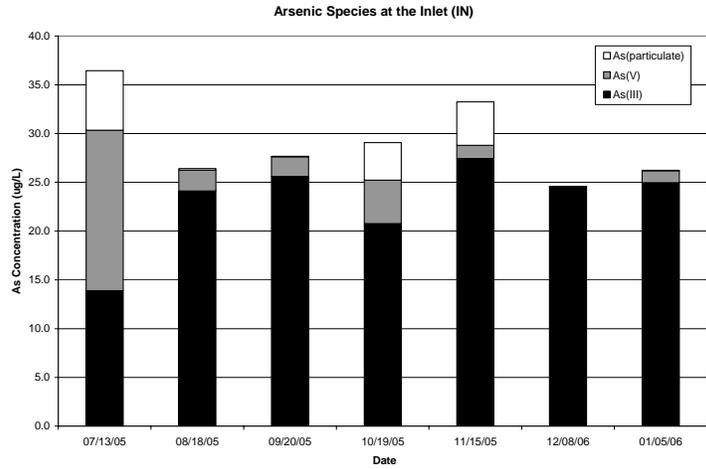
One-half of detection limit used for non-detect samples for calculations.

Duplicate samples included calculations.

(a) On December 8, 2005, arsenic speciation results taken at IN, AC, TA/TB, and TC/TD locations.

presence of elevated TOC levels at 3.2 to 4.8 mg/L (Table 4-7) in raw water. Researchers have reported that Fe(II)-KMnO<sub>4</sub> reaction rates are more rapid than KMnO<sub>4</sub>-DOC interactions (Knocke et al., 1994). Based on the presence of primarily particulate arsenic and iron after the contact tanks, it appears that the elevated TOC levels did not have a significant effect on As(III) and Fe(II) oxidation. Note that KMnO<sub>4</sub> dosages used during the six-month study period ranged from 2.1 to 6.1 mg/L (as KMnO<sub>4</sub>) and averaged 4.8 mg/L. The effects of KMnO<sub>4</sub> dosage on Mn(II) oxidation are discussed in the next subsection.

From July 13, 2005, to January 17, 2006, total arsenic concentrations in the treated water ranged from 2.0 to 29.8 µg/L and averaged 7.9 µg/L (Table 4-6). Soluble arsenic concentrations in the treated water ranged from 2.0 to 6.2 µg/L and averaged 3.5 µg/L. Out of the 26 sampling occasions, total arsenic concentrations in the treated water exceeded the 10-µg/L MCL for a total of 8 times due to particulate breakthrough from the Macrolite<sup>®</sup> filters (Figure 4-9). As shown in Figure 4-10, the elevated total arsenic concentrations were accompanied by elevated total iron concentrations. The iron concentrations in the treated water ranged from <25 to 2,363 µg/L and averaged 323 µg/L, with most existing as particulate iron (Table 4-6). The soluble iron levels were below the method detection limit of <25 µg/L as measured in water samples filtered with 0.45-µm disc filters. On September 7, 2005, the total arsenic concentration in the treated water exceeded 10 µg/L due to low KMnO<sub>4</sub> dosage, which can be seen by the negative ORP readings across the treatment train, resulting in incomplete oxidation of As(III) and Fe(II). A study has shown that Fe(II) complexed with dissolved organic matter (DOM) was very difficult to remove via oxidation and subsequent precipitation of Fe(OH)<sub>3</sub>(s). This was due to the formation of colloidal iron that had a size fraction small enough to pass through 0.2-µm disc filters. However, this phenomenon would be affected by the concentration and nature of the DOM in water (Knocke et al., 1994). The formation of colloidal iron did not appear to be an issue at BSLMHP with primarily particulate iron present after the



**Figure 4-8. Concentrations of Arsenic Species at IN, AC, and TT Sampling Locations**

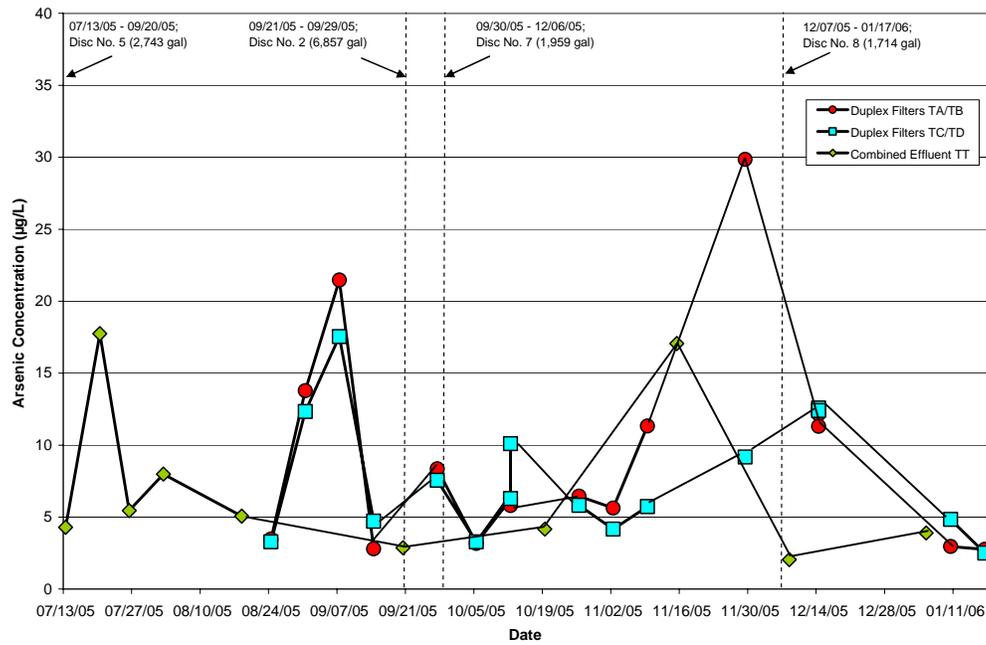


Figure 4-9. Total Arsenic Concentrations at TA/TB, TC/TD, and TT Sampling Locations

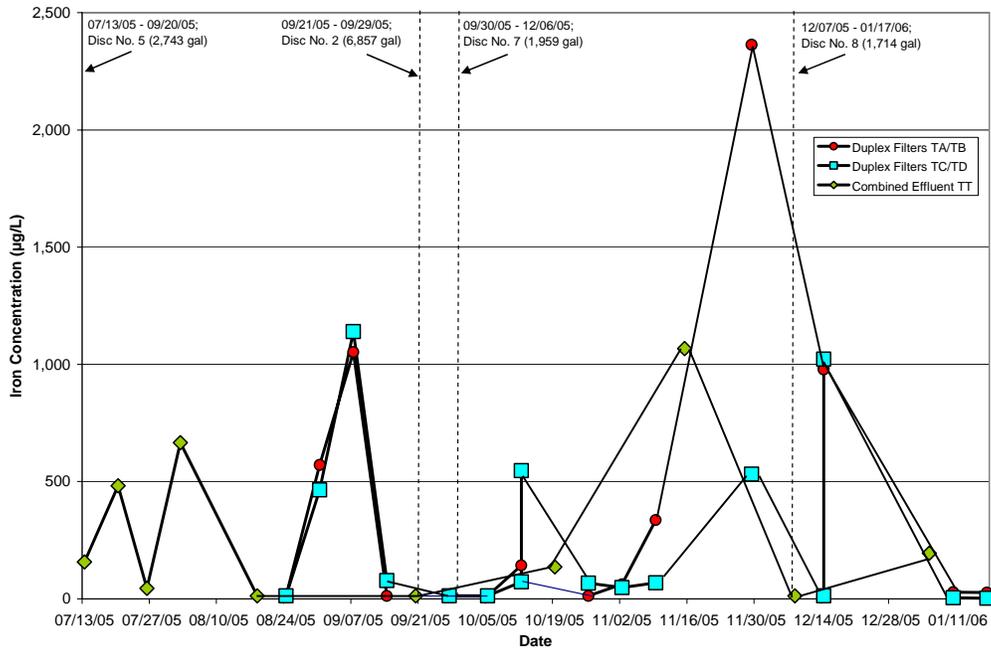


Figure 4-10. Total Iron Concentrations at TA/TB, TC/TD, and TT Sampling Locations

contact tanks and after the Macrolite<sup>®</sup> filters (e.g. a size fraction large enough to be retained by a 0.45 µm disc filter). The increase in particulate iron also corresponded with an increase in particulate arsenic, indicating iron breakthrough from the Macrolite<sup>®</sup> filters.

In order to better control particulate breakthrough from the filtration tanks, the control discs located on top of the two duplex units were replaced twice from Discs No. 5 to No. 7 and, then, from Discs No. 7 to No. 8 during the six-month duration to allow for more frequent backwash. (Note that Disc No. 2 was erroneously installed for a short duration before the mistake was caught and corrected). Table 4-8 lists the disc number, operating duration, total arsenic concentrations exceeding 10 µg/L, and total iron concentrations with arsenic exceeding 10 µg/L. The use of Discs No. 5 and No. 7 resulted in three and four occurrences, respectively, with arsenic concentrations measured as high as 29.8 µg/L and iron concentrations measured as high as 2,363 µg/L. Disc No. 8 was installed on December 7, 2005, and the treated water samples collected during December 7, 2005, through January 17, 2006, contained an average of 4.0 and 194 µg/L of total arsenic and iron, respectively, which were the lowest for the six-month period. However, due to particulate arsenic and iron breakthrough observed on December 14, 2005, control disc No. 8 will be switched out to allow even more frequent backwash during the next six-month period.

**Table 4-8. Control Disc Sizes and Corresponding Occurrences with High Total Arsenic and Iron Concentrations**

Duration	Control Disc	Occurrence	Total Arsenic Concentration Exceeding 10 µg/L			Total Iron Concentration with Arsenic Exceeding 10 µg/L		
			TA/TB	TC/TD	TT	TA/TB	TC/TD	TT
07/13/05–09/20/05	No. 5	1	N/A	N/A	17.7	N/A	N/A	482
		2	13.8	12.3	N/A	571	465	N/A
		3	21.5	17.5	N/A	1,052	1,140	N/A
09/21/05–09/29/05	No. 2 <sup>(a)</sup>	N/A	N/A			N/A		
09/30/05–12/06/05	No. 7	4	N/A	10.1	N/A	N/A	547	N/A
		5	11.3	N/A	N/A	336	N/A	N/A
		6	N/A	N/A	17.1	N/A	N/A	1,067
		7	29.8	N/A	N/A	2,363	N/A	N/A
12/07/05–01/17/06	No. 8	8	12.1	12.6	None	983	1,001	None
			11.3 <sup>(b)</sup>	12.4 <sup>(b)</sup>		978 <sup>(b)</sup>	1,023 <sup>(b)</sup>	

(a) Incorrect disc inadvertently installed and replaced soon after installation.

(b) Field duplicate.

N/A = data not available

**Manganese.** As shown in Table 4-6, total manganese concentrations in raw water ranged from 110 to 430 µg/L and averaged 144 µg/L, which existed primarily in the soluble form at levels ranging from 110 to 145 µg/L and averaging 132 µg/L. The manganese levels in raw water exceeded its secondary MCL of 50 µg/L.

Figure 4-11 shows the concentrations of total and soluble manganese after KMnO<sub>4</sub> addition and after the contact tanks over time. Before November 15, 2005, total manganese levels after the contact tanks ranged from 416 to 1,126 µg/L, 38 to 94% of which was present in the soluble form based on the use of 0.45-µm disc filters. As noted in the figure and Table 4-9, the KMnO<sub>4</sub> dosage was incrementally decreased from the initial level of 3.8 mg/L to 1.4 mg/L, and then increased to 2.6 mg/L by adjusting the

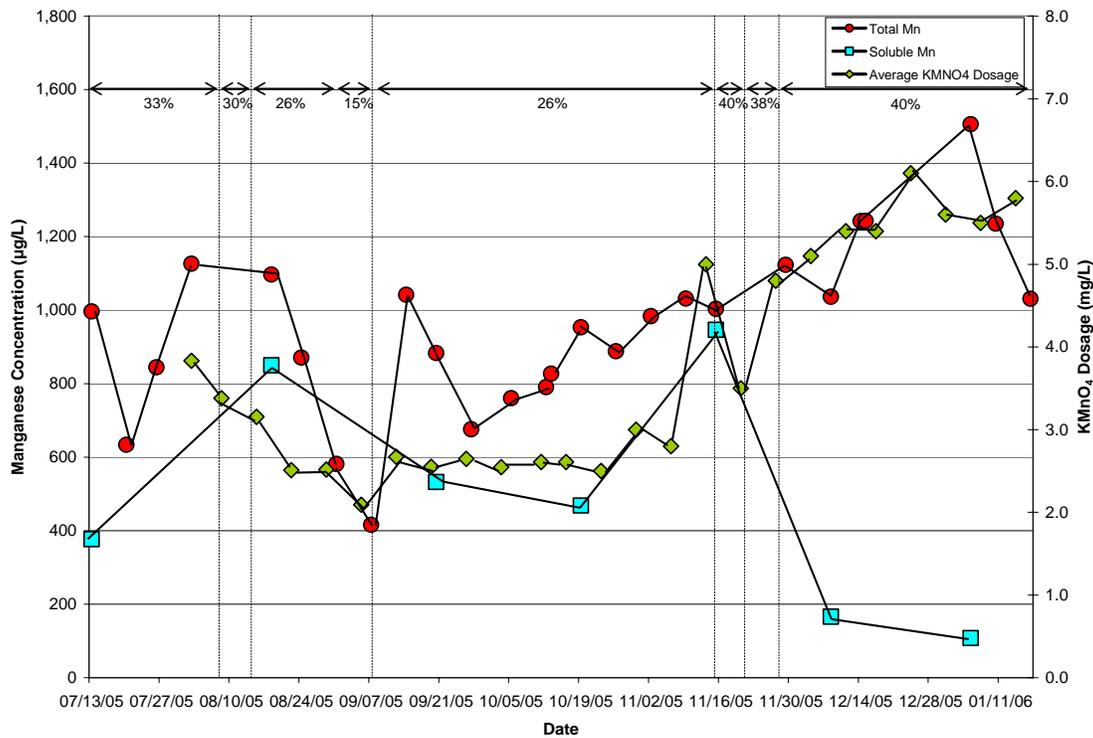


Figure 4-11. Total and Soluble Manganese Concentrations at AC Sampling Location

Table 4-9. Correlations Between Pump Stroke Length, KMnO<sub>4</sub> Dosage, and Total and Soluble Manganese Concentrations

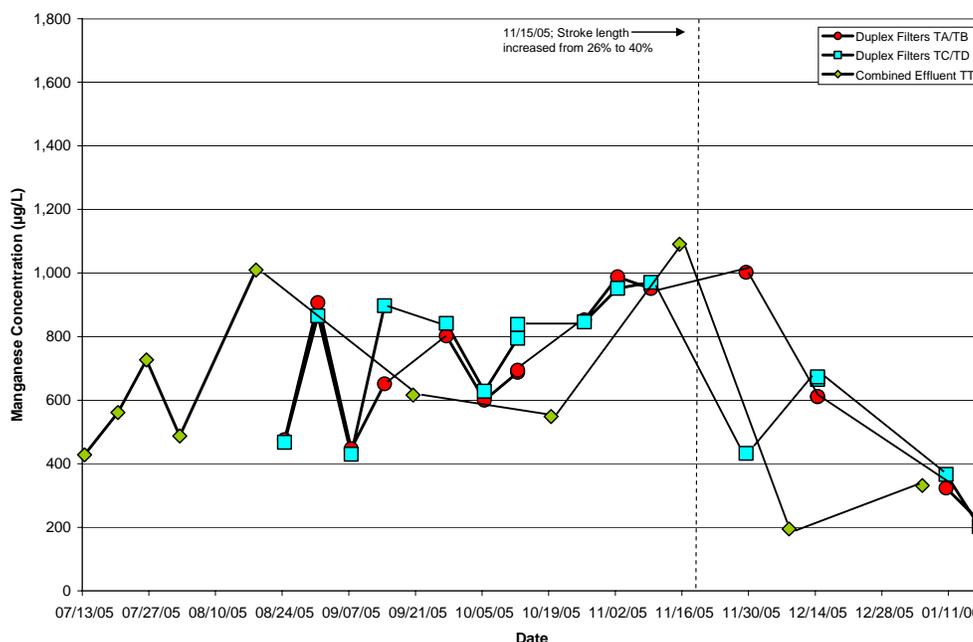
Duration	Stroke Length (%)	Average KMnO <sub>4</sub> Dosage (mg/L)	Total Mn at AC Location (mg/L)	Soluble Mn at AC Location (mg/L)	Total Mn at TA/TB, TC/TD, and TT Location (mg/L)	Soluble Mn at TA/TB, TC/TD, and TT Location (mg/L)
07/13/05 to 08/07/05	33	3.8	634–1,126	337	428–727	391
08/08/05 to 08/13/05	30	3.4	N/A		N/A	
08/14/05 to 08/30/05	26	3.0	871–1,097	850	467–1,010	1,000
08/31/05 to 09/07/05	15	1.4	416–581	N/A	430–906	N/A
09/08/05 to 11/15/05	26	2.6	676–1,042	468–946	548–1,091	535–1,062
11/16/05 to 11/20/05	40	5.4	N/A		N/A	
11/21/05 to 12/04/05	38	3.1	1,123	N/A	432	N/A
12/05/05 to 01/17/06	40	5.6	1,031–1,506	108–166	201–673	138–202

N/A = Data not available

stroke length of the paced-pump from 33 to 15%, then to 26%. The KMnO<sub>4</sub> dosage was decreased from the initial level of 3.8 mg/L because elevated total and soluble manganese levels at 996 (average) and 377 µg/L, respectively, were measured after KMnO<sub>4</sub> addition and thought, at the time, to have been caused by overdosing of KMnO<sub>4</sub>. Decreasing the KMnO<sub>4</sub> dosage from 3.8 to 3.4 and then to 3.0 mg/L did not appear to help reduce the manganese concentrations, with total and soluble levels measured, for example, at 1,097 and 850 µg/L, respectively, on August 18, 2005. A further decrease in KMnO<sub>4</sub> dosage

to 1.4 mg/L helped reduce the total manganese levels, which, however, were still higher than those in raw water at 581 and 416  $\mu\text{g/L}$ , respectively, on August 31 and September 7, 2005. This low level of  $\text{KMnO}_4$  addition also caused significantly elevated arsenic and iron concentrations in the treated water due to incomplete oxidation of As(III) and Fe(II) also discussed in Section 4.5.1. Resuming the  $\text{KMnO}_4$  dosage at 2.6 mg/L returned the total manganese concentrations to 676 to 1,042  $\mu\text{g/L}$ , with most (i.e., 468 to 946  $\mu\text{g/L}$ ) existing in the soluble form, as determined by the use of 0.45- $\mu\text{m}$  disc filters.

The addition of 1.4 mg/L to 3.8 mg/L of  $\text{KMnO}_4$  during July 13 through November 15, 2005, resulted in significantly elevated manganese levels not only after the contact tanks, as discussed above, but also after the Macrolite<sup>®</sup> filters (ranging from 428 to 1,091  $\mu\text{g/L}$  and averaging 722  $\mu\text{g/L}$ , Figure 4-12). Further, manganese in the treated water existed almost entirely (i.e., 535 to 1,062  $\mu\text{g/L}$ ) in the soluble form based on the use of 0.45- $\mu\text{m}$  filter discs for obtaining the soluble fractions.



**Figure 4-12. Total Manganese Concentrations at TA/TB, TC/TD, and TT Sampling Locations**

Mn(II) oxidation by  $\text{KMnO}_4$  is dependent on the  $\text{KMnO}_4$  dosage, pH, temperature, and DOM in raw water. The reaction of  $\text{KMnO}_4$  with Mn(II) is typically rapid and complete at pH values ranging from 5.5 to 9.0. However, elevated DOM levels can increase the  $\text{KMnO}_4$  demand due to competition between these species and resulting kinetic effects (Knocke et al., 1987). Some researchers suggest that DOM can interfere with the formation of  $\text{MnO}_2(\text{s})$  solids by exerting  $\text{KMnO}_4$  demand and, possibly, forming complexes with fractions of Mn(II), thus rendering it less likely to be oxidized (Gregory and Carson, 2003). When modeling the Mn(II) oxidation with  $\text{KMnO}_4$ , Carlson and co-workers (1999) determined that incorporating a term in the model to account for the DOM demand for  $\text{MnO}_4^-$  significantly improved the prediction of the  $\text{MnO}_4^-$  consumption. The incorporation of DOM into the oxidation term to account for complexation between DOM and Mn(II) also was postulated but no data was collected as part of that study. Further, high levels of DOM in source water also can form fine colloidal  $\text{MnO}_2$  particles, which may not be filterable by conventional gravity or pressure filters. Knocke et al. (1991) defined colloidal particles as those passing through 0.20- $\mu\text{m}$  filters and requiring ultrafiltration for removal.

The presence of significantly elevated soluble manganese levels after the contact tanks and after the Macrolite<sup>®</sup> filters, even with the use of insufficient KMnO<sub>4</sub>, prompted the speculation that the soluble manganese measured might, in fact, be colloidal particles that had passed through the 0.45-µm disc filters. Therefore, jar tests were performed on November 7, 2005, to determine if higher KMnO<sub>4</sub> dosages might help overcome the DOM effect and form larger filterable MnO<sub>2</sub> solids in the treated water. Prior to the start of the jar tests, the additional KMnO<sub>4</sub> demand of a Macrolite<sup>®</sup>-treated water sample (to which 3.0 mg/L of KMnO<sub>4</sub> had been added based on the KMnO<sub>4</sub> consumption in the chemical day tank during the week of sampling) was pre-determined by titrating 1 L of the water with a 1-g/L KMnO<sub>4</sub> titrant. After 2.5 mL of the titrant was added, the water being titrated developed a dark yellow color, and was filtered, after about 10 min, with 0.20-µm disc filters to remove any suspended solids including MnO<sub>2</sub>. The filtrate was observed to have a pink color, indicating the presence of KMnO<sub>4</sub> residual.

Five KMnO<sub>4</sub> dosages ranging from 1.0 to 3.0 mg/L were then selected for the jar tests using the same Macrolite<sup>®</sup>-treated water sample mentioned above. (These dosages would be in addition to the KMnO<sub>4</sub> already added to the water to be treated). After 31 min of mixing time (including 1 min at 200 rpm, 19 at 100 rpm, and 11 min at 28 rpm), the water in the jars was filtered separately with 0.20-µm disc filters and analyzed for soluble arsenic, iron, and manganese. Table 4-10 summarizes the results of the jar tests.

**Table 4-10. Jar Test Results for Macrolite<sup>®</sup>-Treated Water**

Parameter	1	2	3	4	5	6
Potassium Permanganate Added (mg/L) <sup>(a)</sup>	0	1.0	1.5	2.0	2.5	3.0
Mixing Time (min)	31	31	31	31	31	31
Initial pH <sup>(b)</sup>	7.70	7.80	7.81	7.71	7.74	7.76
Final pH <sup>(c)</sup> @ 16.8°C	7.68	7.67	7.70	7.62	7.60	7.61
Initial ORP <sup>(b)</sup> @ 16.8°C	283	292	400	440	509	521
Final ORP <sup>(c)</sup>	353	360	363	369	493	515
Residual KMnO <sub>4</sub> (mg/L) <sup>(d)</sup>	0.04	0.01	0.05	0.07	0.35	0.63
As (soluble) <sup>(e)</sup> (µg/L)	5.5	4.5	3.3	3.3	3.2	3.1
Fe (soluble) <sup>(e)</sup> (µg/L)	<25	<25	<25	<25	<25	<25
Mn (soluble) <sup>(e)</sup> (µg/L)	1,090	102	0.8	11.0	399	469

(a) Dosage on top of 3.0 mg/L already added to the water prior to jar tests.

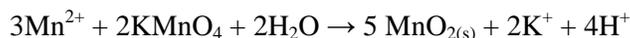
(b) Taken approximately 15 min into jar test.

(c) Taken at end of 31 min jar test.

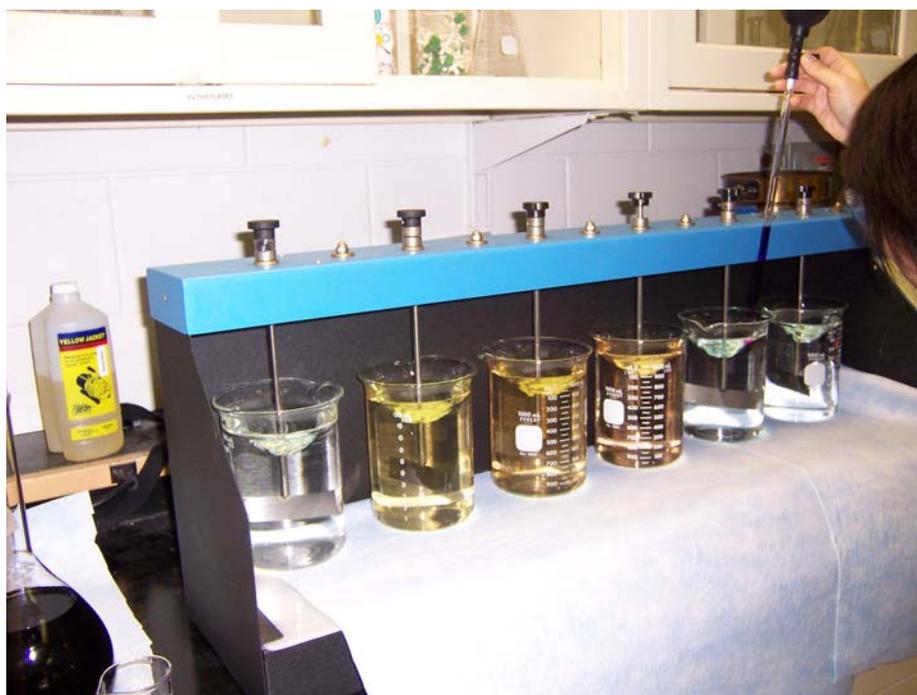
(d) CAIROX<sup>®</sup> Method 103 (DPD Spectrophotometry) for determination of KMnO<sub>4</sub> residual.

(e) Filtered with 0.20-µm filters.

During mixing, jars No. 2 to 4 formed large brown flocs in a pale to dark yellow solution (Figure 4-13). Jars No. 5 to 6 had smaller brown flocs in a dark copper solution. As shown in Table 4-10, the soluble iron levels in all jars were below the method detection limit of 25 µg/L, suggesting that effective oxidation and removal of iron had already been achieved prior to the jar tests. Soluble arsenic levels decreased slightly from 5.5 µg/L to 3.1 µg/L in jar No. 6 (the one with the highest KMnO<sub>4</sub> dosage 3.0 mg/L). Only soluble manganese concentrations varied significantly, decreasing from 1,090 µg/L in jar No. 1 to <1 µg/L in jar No. 3 and then increasing to 469 µg/L in jar No. 6. Knocke et al. (1990) reported that the kinetics for Fe(II) oxidation are faster than for Mn(II) oxidation when KMnO<sub>4</sub> is used as the oxidant. The relevant stoichiometric equations are shown as follows:



In the control sample, the soluble manganese level was high due to the slower Mn(II) oxidation kinetics and the presence of DOM as discussed above. The 1,090  $\mu\text{g/L}$  of “soluble” manganese in the control sample confirmed that the manganese most likely was present as colloidal particles since the sample analyzed had already been filtered with 0.2  $\mu\text{m}$  disc filters. Increasing the  $\text{KMnO}_4$  dosage to 1.5 mg/L (on top of the 3.0 mg/L already added to the water prior to the jar tests) appeared to be sufficient to overcome the effects of DOM, allowing filterable manganese particles to form. As a result, only 0.8  $\mu\text{g/L}$  of manganese that passed through the 0.2- $\mu\text{m}$  filters was reported as “soluble” manganese. Further, increasing the  $\text{KMnO}_4$  dosage up to 3 mg/L increased the soluble manganese level up to 469  $\mu\text{g/L}$ , suggesting that excess  $\text{KMnO}_4$  was present in the treated water. The presence of  $\text{KMnO}_4$  was supported by the elevated residual  $\text{KMnO}_4$  levels and the elevated ORP readings (see results of jars No. 4 and 5).



**Figure 4-13. Jar Test Setup**

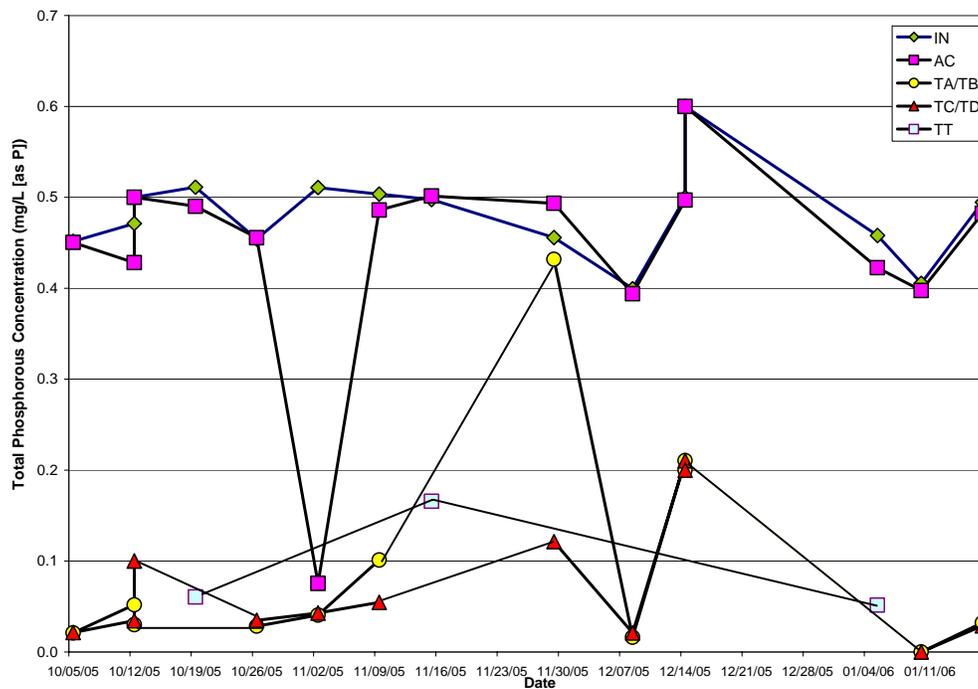
Based on the jar tests results, it was determined that an additional 1.5 mg/L of  $\text{KMnO}_4$  was needed to attain filterable manganese solids. Therefore, the  $\text{KMnO}_4$  dosage to the treatment system was increased on November 15, 2005 for a target dosage of 4.5 mg/L. The actual dosage after adjusting the stroke length from 26 to 40% was 5.4 mg/L (Table 4-9). After the increase in dosage, manganese was present primarily in the particulate form, with concentrations ranging from 1,031 to 1,506  $\mu\text{g/L}$ . The soluble manganese was decreased significantly to 108 to 166  $\mu\text{g/L}$  (Figure 4-11). (Note that as before, 0.45- $\mu\text{m}$  filters were used to obtain these treatment results). After November 15, 2005, the speciation results indicated that approximately 7 to 16% was present as soluble manganese in the Macrolite<sup>®</sup> treated water: the total manganese concentrations ranged from 201 to 673  $\mu\text{g/L}$  and the soluble manganese concentrations ranged from 138 to 202  $\mu\text{g/L}$ . Based on an average soluble manganese concentration of 177  $\mu\text{g/L}$  and total manganese concentration of 673  $\mu\text{g/L}$ , particulate manganese breakthrough of up to 496  $\mu\text{g/L}$  was experienced from the Macrolite<sup>®</sup> filters. In the next six-month period, further fine-tuning will be made to the  $\text{KMnO}_4$  dosing to determine if soluble manganese may be further reduced to less than the Secondary Maximum Contaminant Level (SMCL) of 50  $\mu\text{g/L}$ .

**TOC.** TOC levels in raw water were elevated, ranging from 3.2 to 4.8 mg/L.  $\text{KMnO}_4$  was used as the oxidant to prevent the formation of disinfection byproducts. Before November 15, 2005, the effluent TOC levels ranged from 3.8 to 4.8 mg/L and there was little or no TOC removal across the treatment train. After November 15, 2005, the influent TOC level was 3.2 mg/L (average) and the effluent TOC level was 3.0 mg/L (average) with approximately 6% removal. Research has shown that only minimal organic carbon removal occurs (at less than 10%) via  $\text{KMnO}_4$  oxidation in source water containing Mn(II) and DOC (Salbu and Steinnes, 1995; Knocke et al., 1990). However, significant DOC removal with colloidal iron particles produced by Fe(II) oxidation was observed (Knocke et al., 1994). The complexation of iron with organic carbon does not appear to be a significant factor at the BSLMHP site as discussed previously.

**Other Water Quality Parameters.** DO levels remained low across the treatment train (with average values ranging from 1.2 to 0.9 mg/L), but ORP values increased across the treatment train (ranging from -76 to -23 mV before versus 1 to 196 mV after  $\text{KMnO}_4$  addition). There were two outliers on September 7 and October 26, 2005, where the ORP values after the contact tanks were negative. The ORP on September 7, 2005, was negative because the stroke on the  $\text{KMnO}_4$  pump was turned down to 15% on August 30, 2005. The pH in raw water had an average value of 7.3 and the pH in the treated water had an average value of 7.3. Average alkalinity results ranged from 366 to 369 mg/L (as  $\text{CaCO}_3$ ) across the treatment train. Average total hardness results ranged from 315 to 319 mg/L (as  $\text{CaCO}_3$ ) across the treatment train (the total hardness is the sum of calcium hardness and magnesium hardness). The water had an almost even split of calcium and magnesium hardness. Fluoride concentrations were 0.2 mg/L in raw water and after contact tanks and were not affected by the Macrolite<sup>®</sup> filtration. The average nitrate concentration was <0.05 mg/L (as N) across the treatment train. There was no detection of sulfate and the silica concentrations remained at approximately 24 mg/L (as  $\text{SiO}_2$ ) across the treatment train.

Orthophosphate was analyzed between July 13, 2005, and October 5, 2005, and there was no detection. However, total phosphorous analyzed between October 12, 2005 and January 17, 2006, showed an elevated average of 0.5 mg/L (as P) in raw water and 0.1 mg/L (as P) in the treated water (Figure 4-14). This indicates a removal rate of approximately 80% most likely through adsorption onto iron solids. The elevated total phosphorous levels were further confirmed by analyzing a raw water sample taken on December 14, 2005, for the various phosphorous species according to EPA Method 365.3 by Sierra Environmental Monitoring, Inc. It was determined that the total phosphorous level in raw water was at 0.58 mg/L (as P), which was present primarily as total hydrolyzable phosphorous at 0.51 mg/L (as P). According to the EPA Method 365.3, total hydrolyzable phosphorous includes both polyphosphorous and some organic phosphorous. It also was later confirmed that no organopesticides were present in source water by EPA Method 507. There were other potential sources for elevated phosphorous in groundwater. Based on research conducted by the Sauk River Watershed District, the Sauk River and Big Sauk Lake have sediment, phosphorous, and nitrates caused by non-point source discharges from septic systems, agriculture, and urban runoff (Post, 2005). The historical monitoring data for the surface water of Big Sauk Lake shows a maximum total phosphorous level of 0.4 mg/L (as P) (Big Sauk Lake River Watershed District, 2006) and the Big Sauk Lake is located approximately 1000 ft from the BSLMHP wellhouse.

**4.5.2 Backwash Water Sampling.** Table 4-11 summarizes the analytical results from the six backwash water sampling events. For the first three sampling events, only pH, turbidity, TDS, and soluble As, Fe, and Mn were analyzed for the grab samples collected at the backwash water discharge line. Soluble arsenic concentrations in the backwash water ranged from 3.5 to 8.5  $\mu\text{g/L}$ ; soluble iron concentrations ranged from <25 to 63  $\mu\text{g/L}$ ; and soluble manganese concentrations ranged from 560 to 736  $\mu\text{g/L}$  based on the use of 0.45- $\mu\text{m}$  filters. Starting from November 15, 2005, TSS and total As, Fe, and Mn also were analyzed for the composite sample collected using the modified backwash procedure discussed in Section 3.3.4. After the modified backwash procedure was implemented, total arsenic



**Figure 4-14. Total Phosphorous Concentrations at IN, AC, TA/TB, TC/TD and TT Sampling Locations**

concentrations in the backwash water ranged from 114 to 417  $\mu\text{g/L}$ ; total iron concentrations ranged from 14,069 to 77,641  $\mu\text{g/L}$ ; and total manganese concentrations ranged from 1,595 to 16,178  $\mu\text{g/L}$ . Note that November 15, 2005, BW2 data had uncharacteristically high total and soluble As and Fe, and, therefore, were excluded from all calculations. TSS levels in the backwash water ranged from 102 to 210  $\text{mg/L}$  and averaging 154  $\text{mg/L}$  (excluding November 15, 2005 BW2 data that had uncharacteristically high As and Fe and the January 10, 2006, BW2 data that had uncharacteristically low TSS). Using 130 gal of backwash water produced, this equates to approximately 0.17 lb of solids generated per backwash event including  $4.4 \times 10^{-4}$  lb of arsenic, 0.08 lb of iron, and 0.01 lb manganese.

**4.5.3 Distribution System Water Sampling.** The results of the distribution system sampling are summarized in Table 4-12. The main differences observed before and after the operation of the system were decreases in arsenic, iron, and manganese concentrations at each of the three sampling locations. Arsenic concentrations in the baseline samples ranged from 15.3 to 26.3  $\mu\text{g/L}$ . Since the treatment system started operation, arsenic levels in the distribution system samples ranged from 3.6 to 14.2  $\mu\text{g/L}$  with an average of 6.6  $\mu\text{g/L}$ . Arsenic concentrations mirrored the treatment results after the Macrolite<sup>®</sup> filters, except for an outlier at 24.1  $\mu\text{g/L}$  on January 17, 2006, when the homeowner did not sufficiently flush the tap the night before sampling. Total arsenic concentrations exceeded 10  $\mu\text{g/L}$  at all three sampling locations on September 7, 2005, due to particulate arsenic and iron breakthrough from the Macrolite<sup>®</sup> filters described in Section 4.4.2. Iron concentrations in the baseline samples were high, ranging from 2.1 to 5.0  $\text{mg/L}$ . Since system startup, iron levels in the distributed water decreased significantly to an average value of 128  $\mu\text{g/L}$  (not including the outlier at DS1 on January 17, 2006). Particulate breakthrough was observed on September 7, November 29, and December 15, 2005 with elevated iron concentrations ranging from 532 to 2,363  $\mu\text{g/L}$  after the Macrolite<sup>®</sup> filters. Iron concentrations in the distribution system during those days ranged from <25 to 279  $\mu\text{g/L}$ , indicating

**Table 4-11. Backwash Water Sampling Results**

Sampling Event		BW1												BW2											
		Tank A/B												Tank C/D											
		KMnO <sub>4</sub> Dosage	Control Disc	pH	Turbidity	TDS	TSS	Total As	Soluble As	Particulate As	Total Fe	Soluble Fe	Total Mn	Soluble Mn	pH	Turbidity	TDS	TSS	Total As	Soluble As	Particulate As	Total Fe	Soluble Fe	Total Mn	Soluble Mn
No.	Date	mg/L	No.	S.U.	NTU	mg/L	µg/L						S.U.	NTU	mg/L	µg/L									
1	09/08/05	2.6	5	7.2	170	576	NS	NS	3.9	NS	NS	<25	NS	624	7.3	120	544	NS	NS	3.5	NS	NS	<25	NS	560
2	09/20/05	2.6	5	7.3	160	550	NS	NS	3.6	NS	NS	<25	NS	624	7.3	17	368	NS	NS	8.5	NS	NS	<25	NS	736
3	10/12/05 <sup>(a)</sup>	2.6	7	7.3	120	356	NS	NS	4.4	NS	NS	<25	NS	685	7.3	410	350	NS	NS	4.3	NS	NS	63	NS	656
4	11/15/05 <sup>(b, c)</sup>	2.6	7	7.5	NS	54	102	329	6.9	322	63,108	163	1,595	836	7.5	NS	346	348	1,325	206	1,119	214,211	29,992	3,835	1,175
5	12/08/05	5.6	8	7.4	NS	224	210	417	0.5	416	77,641	201	16,178	350	7.6	NS	334	175	397	2.9	394	75,485	39	14,159	348
6	01/10/06	5.6	8	7.4	NS	360	130	363	3.3	360	43,384	128	12,265	341	7.6	NS	326	16	114	5.3	109	14,069	304	4,016	376

TDS = total dissolved solids; TSS = total suspended solids; NS = not sampled.

- (a) Manual backwash performed after Tank A/B had just been backwashed; less particles visually observed
- (b) Samples taken on November 15, 2005 re-analyzed with similar results for both samples on this date.
- (c) Modified backwash procedures implemented starting November 15, 2005.

**Table 4-12. Distribution Sampling Results**

Sampling Events		As at Entry Point	DS1								DS2								DS3							
			Stagnation Time	pH	Alkalinity	As	Fe	Mn	Pb	Cu	Stagnation Time	pH	Alkalinity	As	Fe	Mn	Pb	Cu	Stagnation Time	pH	Alkalinity	As	Fe	Mn	Pb	Cu
No.	Date	µg/L	hr	S.U.	mg/L	µg/L					hr	S.U.	mg/L	µg/L					hr	S.U.	mg/L	µg/L				
BL1	02/16/05	NA	7.0	7.2	382	24.3	2,649	128	0.6	4.1	8.3	7.4	374	19.8	2,792	129	0.6	0.2	NS	NS	NS	NS	NS	NS	NS	NS
BL2	03/23/05	NA	6.0	7.3	362	21.9	2,175	130	0.4	2.2	8.3	7.4	367	26.2	4,986	147	0.3	2.5	7.3	7.5	376	26.3	2,590	128	<0.1	1.9
BL3	04/19/05	NA	6.2	7.0	377	25.3	2,878	141	2.4	3.9	10.0	7.2	395	15.3	2,137	127	1.6	3.4	8.4	7.4	386	24.6	2,751	133	0.2	0.4
BL4	05/23/05	NA	5.8	7.3	384	25.7	2,578	124	0.5	0.7	7.3	7.3	370	24.2	2,639	123	<0.1	0.4	8.8	7.3	379	22.6	2,649	119	0.1	0.9
1	07/26/05	5.5	7.3	7.2	365	5.1	73	722	0.5	0.4	9.3	7.3	374	5.4	84	617	0.4	0.2	9.3	7.3	370	6.3	162	612	0.4	0.6
2	09/07/05	21.5/ 17.5	8.5	7.4	356	14.2	52	438	0.3	0.2	9.0	7.5	352	12.7	<25	516	<0.1	1.7	8.0	7.6	365	13.9	84	525	<0.1	1.4
3	09/27/05	8.4/ 7.6	8.3	7.3	370	4.3	72	687	2.1	11.0	7.3	7.4	361	5.1	127	717	0.2	<0.1	9.5	7.4	374	4.2	98	659	1.1	1.0
4	11/02/05	5.6/ 4.2	12.5	7.6	361	6.8	<25	976	0.2	8.8	7.0	7.6	352	7.9	142	950	<0.1	0.2	9.3	7.6	365	8.5	37	935	0.2	0.3
5	11/29/05	9.2	8.0	7.4	365	4.1	266	367	0.9	6.2	6.0	7.5	365	3.6	57	369	0.1	0.2	9.3	7.5	361	3.7	222	478	1.1	2.4
6	12/15/05	11.7/ 12.5	11.3	7.5	374	4.1	57	400	1.2	3.9	8.0	7.6	374	5.7	184	443	0.8	0.2	9.0	7.5	374	6.3	279	468	1.0	0.7
7	01/17/06	2.8/ 2.5	9.0	7.5	383	24.1	1,999	923	1.0	21.8	8.5	7.5	383	4.9	187	267	0.2	0.7	7.5	7.6	383	4.9	342	226	4.7	3.2

NS = not sampled; NA = not analyzed/applicable.

settling of iron solids within the distribution system piping. On January 17, 2006, due to insufficient flushing of the sampling tap, the iron concentration at DS1 was 1,999 µg/L while iron concentrations after the Macrolite® filters were very close to the detection limit of 25 µg/L. Manganese levels in the distribution system baseline samples averaged 130 µg/L and increased to an average of 569 µg/L after the treatment system became operational. The manganese concentrations in the distribution system mirrored the results after the Macrolite® filters.

There was no major change in pH values in the distribution system, which ranged from 7.0 to 7.5 before system startup and 7.2 to 7.6 after startup. Alkalinity levels in the distribution system ranged from 362 to 395 mg/L (as CaCO<sub>3</sub>) before and 352 to 383 (as CaCO<sub>3</sub>) after.

Lead and copper levels in the distribution system did not appear to have been affected by the operation of the arsenic treatment system. Lead levels in the distribution system ranged from <0.1 to 4.7 µg/L with no samples exceeding the action level of 15 µg/L. Copper concentrations ranged from <0.1 to 21.8 µg/L with no samples exceeding the 1,300 µg/L action level.

## **4.6 System Cost**

The cost of the system was evaluated based on the capital cost per gpm (or gpd) of design capacity and the O&M cost per 1,000 gal of water treated. This required the tracking of the capital cost for equipment, engineering, and installation cost and the O&M cost for chemical supply, electrical power use, and labor. However, the cost associated with improvements to the building and any other discharge-related infrastructure were not included in the treatment system cost. While not included in the scope of the demonstration project, these activities were funded by the demonstration host site.

**4.6.1 Capital Cost.** The capital investment was \$63,547, which included \$22,422 for equipment, \$20,227 for site engineering, and \$20,898 for installation. Table 4-13 presents the breakdown of the capital cost as provided by the vendor in its proposal to Battelle dated February 17, 2005. The equipment cost was about 35% of the total capital investment, which included the CP-213f filtration tanks, Macrolite® media, contact tanks, process valves and piping, instrumentation and controls, a chemical feed system (including a storage tank with a secondary containment), additional sample taps and totalizer/meters, shipping, and equipment assembly labor.

The engineering cost included the cost for preparing a process design report and required engineering plans, including a general arrangement drawing, piping and instrumentation diagrams (P&IDs), interconnecting piping layouts, tank fill details, an electrical on-line diagram, and other associated drawings. After certification by a Minnesota-registered professional engineer (PE), the plans were submitted to the MDH for permit review and approval (Section 4.3.1). The engineering cost was \$20,227, which was 32% of the total capital investment.

The installation cost included the cost for labor and materials for system unloading and anchoring, plumbing, and mechanical and electrical connections (Section 4.3.3). The installation cost was \$20,898 or 33% of the total capital investment.

Using the system's rated capacity of 20 gpm (or 28,800 gpd), the capital cost was normalized to be \$3,177/gpm (or \$2.21/gpd). The capital cost of \$63,547 was converted to an annualized cost of \$5,998/year using a capital recovery factor of 0.09439 based on a 7% interest rate and a 20-year return. Assuming that the system was operated 24 hours a day, 7 days a week at the design flow rate of 20 gpm to produce 10,500,000 gal of water per year, the unit capital cost would be \$0.57/1,000 gal. However, since the system operated an average of 3.4 hr/day at just under 4.4 gpm (see Table 4-4), producing 863,470 gal of water during the six-month period, the unit capital cost was increased to \$3.47/1000 gal at this reduced rate of production.

**Table 4-13. Summary of Capital Investment for BSLMHP Treatment System**

Description	Quantity	Cost	% of Capital Investment Cost
<i>Equipment Cost</i>			
Media and Tanks	1	\$8,549	–
Process Valves and Piping	1	\$1,935	–
Chemical Feed	1	\$1,150	–
Chemical Storage and Secondary Containment	1	\$680	–
Instrumentation and Controls	1	\$1,079	–
Additional Flowmeter/Totalizers	1	\$359	–
Shipping	–	\$750	–
Labor	–	\$7,920	–
<b>Equipment Total</b>	–	<b>\$22,422</b>	<b>35%</b>
<i>Engineering Cost</i>			
Labor	–	\$15,620	–
Travel	–	\$1,750	–
Subcontractor	–	\$2,857	–
<b>Engineering Total</b>	–	<b>\$20,227</b>	<b>32%</b>
<i>Installation Cost</i>			
Labor	–	\$5,000	–
Travel	–	\$2,913	–
Subcontractor	–	\$12,985	–
<b>Installation Total</b>	–	<b>\$20,898</b>	<b>33%</b>
<b>Total Capital Investment</b>	–	<b>\$63,547</b>	<b>100%</b>

**4.6.2 Operation and Maintenance Cost.** The O&M cost primarily included cost associated with chemical supply, electricity consumption, and labor (Table 4-14). The usage rate for the KMnO<sub>4</sub> stock solution was approximately 7.5 gal or 100 lb/yr. Incremental electrical power consumption was calculated for the chemical feed pump. The power demand was calculated based on the total operational hours throughout the duration of the six-month study, the chemical feed pump horsepower, and the unit cost from the utility bills. The routine, non-demonstration related labor activities consumed about 5 min per day, 5 days a week, as noted in Section 4.4.4. Based on this time commitment and a labor rate of \$21/hr, the labor cost was \$0.27/1,000 gal of water treated. In sum, the total O&M cost was approximately \$0.43/1,000 gal. The O&M cost will be verified during the next reporting period.

**Table 4-14. O&M Cost for BSLMHP, MN Treatment System**

<b>Cost Category</b>	<b>Value</b>	<b>Assumption</b>
Projected Volume Processed (gal)	863,470	From 07/13/05 through 01/17/06 (see Table 4-4)
<b><i>Chemical Usage</i></b>		
Chemical Unit Price (\$/lb)	\$2.07	97% KMnO <sub>4</sub> in a 55-lb pail (approximately 4 gal)
Total Chemical Consumption (lb)	50	7.5 gal or 100 lb of KMnO <sub>4</sub> per year
Chemical Usage (lb/1,000 gal)	0.058	
Total Chemical Cost (\$)	\$103.5	
Unit Chemical Cost (\$/1,000 gal)	\$0.12	
<b><i>Electricity</i></b>		
Electricity Unit Cost (\$/kwh)	0.067	
Estimated Electricity Usage (kwh)	515	Calculated based on 617 hr of operation of a 0.17-hp chemical feed pump
Estimated Electricity Cost (\$)	\$34.54	
Estimated Power Use (\$/1,000 gal)	\$0.04	
<b><i>Labor</i></b>		
Average Weekly Labor (hr)	0.42	5 min/day; 5 days a week
Total Labor Hours (hr)	11	26 weeks
Total Labor Cost (\$)	\$231	Labor rate = \$21/hr
Labor Cost (\$/1,000 gal)	\$0.27	
<b>Total O&amp;M Cost/1,000 gal</b>	<b>\$0.43</b>	-

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**APPENDIX A**  
**OPERATIONAL DATA**

**US EPA Arsenic Demonstration Project at BSLMHP, MN – Daily System Operation Log Sheet**

Week No.	Date	Time	New Well		Volume to Treatment		Pressure Tanks		Pressure Filtration					Volume to Distribution		Backwash		KMnO <sub>4</sub> Application		
			Hour Meter (hr)	Daily Operation (hr)	Daily Volume (gal)	Average Flowrate (gpm)	Pressure Tank 1 (psig)	Pressure Tank 2 (psig)	IN (psig)	TA/TB (psig)	TC/TD (psig)	OUT (psig)	ΔP Across System (psig)	Flowrate (gpm)	Daily Volume (gal)	No. of Tanks Backwashed	Wastewater Produced (gal)	KMnO <sub>4</sub> Tank Level (in)	Average KMnO <sub>4</sub> Dose (mg/L)	
1	07/13/05	21:13	NM	NA	NA	NA	NM	NM	42	NM	NM	30	12	NM	NA	NM	NA	NM	NA	
	07/14/05	20:10	NM	NA	6,980	NA	NM	NM	54	NM	NM	37	17	NM	7,000	1	110	NM	NA	
	07/15/05	20:00	NM	NA	6,880	NA	NM	NM	40	NM	NM	30	10	NM	6,700	2	240	NM	NA	
	07/16/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	NA	
	07/17/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	NA	
2	07/18/05	18:45	NM	NA	NA	NA	NM	NM	58	NM	NM	45	13	NM	NA	NM	NA	NM	NA	
	07/19/05	19:10	NM	NA	9,125	NA	NM	NM	40	NM	NM	36	4	NM	8,900	3	350	NM	NA	
	07/20/05	19:00	NM	NA	11,075	NA	NM	NM	45	NM	NM	22	23	NM	10,800	3	440	NM	NA	
	07/21/05	18:30	NM	NA	14,470	NA	NM	NM	45	NM	NM	35	10	NM	14,300	4	490	NM	NA	
	07/22/05	20:00	NM	NA	7,680	NA	NM	NM	48	NM	NM	42	6	NM	7,400	3	360	NM	NA	
	07/23/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	NA	
07/24/05	NM	NM	NA	NA	NA	NA	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	NA		
3	07/25/05	19:30	NM	NA	14,250	NA	NM	NM	47	NM	NM	45	2	NM	13,900	4	470	NM	NA	
	07/26/05	20:10	NM	NA	4,020	NA	NM	NM	41	NM	NM	40	1	NM	3,900	1	130	NM	NA	
	07/27/05	23:15	NM	NA	4,030	NA	NM	NM	58	NM	NM	55	3	NM	3,900	1	110	NM	NA	
	07/28/05	20:15	NM	NA	4,180	NA	NM	NM	41	NM	NM	40	1	NM	3,900	2	240	NM	NA	
	07/29/05	18:15	NM	NA	3,340	NA	NM	NM	56	NM	NM	53	3	NM	3,200	1	120	NM	NA	
	07/30/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NM	NM	NM	NM	NA	NM	NA	
	07/31/05	NM	NM	NA	NA	NA	NA	NM	NM	NM	NM	NM	NM	NM	NM	NM	NA	NM	NA	
4	08/01/05	19:05	NM	NA	18,670	NA	52	72	58	NM	NM	48	10	NM	18,100	5	710	30.0	NA	
	08/02/05	20:30	NM	NA	6,057	NA	46	72	42	NM	NM	40	2	NM	5,900	2	240	29.6	3.8	
	08/03/05	23:55	NM	NA	4,733	NA	45	72	41	NM	NM	38	3	NM	4,500	1	120	29.3		
	08/04/05	23:55	NM	NA	3,635	NA	53	72	49	NM	NM	46	3	NM	3,600	1	120	28.9		
	08/05/05	22:00	NM	NA	3,985	NA	45	72	42	NM	NM	40	2	NM	3,700	2	240	28.7		
	08/06/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NM	NM	NM	NM	NA	NM		NA
	08/07/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NM	NM	NM	NM	NA	NM		NA
08/08/05	21:30	NM	NA	12,020	NA	60	72	58	NM	NM	50	8	NM	11,600	4	490	27.8			
5	08/09/05 <sup>(a, b)</sup>	21:30	NM	NA	7,195	NA	55	72	55	44	38	42	13	NM	5,100	13	1,720	27.4	3.4	
	08/10/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NM	NM	NM	NM	NA	NM		NA
	08/11/05 <sup>(c)</sup>	18:00	NM	NA	4,885	NA	50	46	42	40	34	40	2	NM	4,200	6	740	27.1		
	08/12/05	20:30	NM	NA	5,200	NA	56	50	48	38	30	37	11	NM	5,000	1	150	26.8		
	08/13/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM		NA
	08/14/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM		NA
6	08/15/05	21:00	NM	NA	15,090	NA	54	49	46	42	34	40	6	NM	14,600	4	490	25.8	3.2	
	08/16/05	21:30	NM	NA	5,410	NA	45	40	43	38	30	39	4	NM	5,100	1	120	25.4		
	08/17/05	20:00	NM	NA	3,360	NA	55	54	55	30	22	30	25	NM	3,400	2	320	25.3		
	08/18/05	19:15	NM	NA	5,860	NA	49	45	42	36	30	36	6	NM	5,530	1	130	24.9		
	08/19/05	20:30	NM	NA	4,620	NA	54	50	47	42	38	43	4	NM	4,205	3	380	24.6		
	08/20/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM		NA
08/21/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	NA		
7	08/22/05	20:20	NM	NA	11,460	NA	54	51	48	45	40	42	6	NM	10,315	6	790	23.9	2.5	
	08/23/05	22:10	NM	NA	5,140	NA	60	59	50	46	40	47	3	NM	5,110	1	120	23.8		
	08/24/05	21:00	NM	NA	4,400	NA	46	44	42	40	34	40	2	NM	3,930	3	370	23.5		
	08/25/05	21:15	NM	NA	3,680	NA	48	44	40	34	30	33	7	NM	3,640	0	0	23.4		
	08/26/05	NM	NM	NA	2,970	NA	53	50	48	43	40	46	2	NM	2,535	3	380	23.1		
	08/27/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM		NA
	08/28/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM		NA

**US EPA Arsenic Demonstration Project at BSLMHP, MN – Daily System Operation Log Sheet (continued)**

Week No.	Date	Time	New Well		Volume to Treatment		Pressure Tanks		Pressure Filtration					Volume to Distribution		Backwash		KMnO <sub>4</sub> Application		
			Hour Meter (hr)	Daily Operation (hr)	Daily Volume (gal)	Average Flowrate (gpm)	Pressure Tank 1 (psig)	Pressure Tank 2 (psig)	IN (psig)	TA/TB (psig)	TC/TD (psig)	OUT (psig)	ΔP Across System (psig)	Flowrate (gpm)	Daily Volume (gal)	No. of Tanks Backwashed	Wastewater Produced (gal)	KMnO <sub>4</sub> Tank Level (in)	Average KMnO <sub>4</sub> Dose (mg/L)	
8	08/29/05	21:00	NM	NA	13,980	NA	50	48	44	40	32	40	4	NM	13,775	5	660	22.4	2.5	
	08/30/05	21:00	NM	NA	7,290	NA	48	43	42	40	30	39	3	NM	5,900	4	520	22.0		
	08/31/05	22:30	NM	NA	4,530	NA	55	50	49	48	40	46	3	NM	4,095	2	250	21.9		
	09/01/05	21:30	NM	NA	3,240	NA	48	46	43	40	32	40	3	NM	3,125	1	140	21.8		
	09/02/05	21:15	NM	NA	3,190	NA	45	42	40	38	36	38	2	NM	3,120	2	200	21.6		
	09/03/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM		NA
	09/04/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM		NA
9	09/05/05	20:00	NM	NA	15,955	NA	51	50	46	42	35	44	2	NM	14,625	7	850	21.4	2.1	
	09/06/05	21:30	NM	NA	5,155	NA	50	49	45	43	34	42	3	NM	4,725	3	390	21.2		
	09/07/05	20:15	NM	NA	4,320	NA	50	46	40	40	32	40	0	NM	4,205	1	140	21.1		
	09/08/05	21:15	NM	NA	4,750	NA	60	55	59	55	48	54	5	NM	4,275	3	390	20.9		
	09/09/05	20:30	NM	NA	5,010	NA	54	50	55	52	46	50	5	NM	5,040	1	120	20.6		
	09/10/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM		NA
	09/11/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM		NA
10	09/12/05	21:00	NM	NA	10,840	NA	46	44	41	36	30	38	3	NM	9,645	5	660	20.1	2.7	
	09/13/05	22:15	NM	NA	4,675	NA	45	43	45	40	35	44	1	NM	4,255	2	270	19.9		
	09/14/05	23:50	NM	NA	4,990	NA	48	48	43	41	34	41	2	NM	4,435	3	390	19.6		
	09/15/05	22:00	NM	NA	3,020	NA	60	60	55	52	46	52	3	NM	2,925	0	0	19.5		
	09/16/05	21:00	NM	NA	2,715	NA	55	53	52	50	45	50	2	NM	2,700	1	130	19.4		
	09/17/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM		NA
	09/18/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM		NA
11	09/19/05	20:00	NM	NA	13,405	NA	51	50	46	42	34	42	4	NM	12,265	6	770	18.7	2.6	
	09/20/05	17:30	NM	NA	4,860	NA	45	48	45	52	46	44	1	NM	4,095	5	660	18.5		
	09/21/05 <sup>(a)</sup>	20:00	NM	NA	4,940	NA	62	60	55	46	43	52	3	NM	4,495	2	280	18.2		
	09/22/05	20:15	NM	NA	4,665	NA	60	58	53	55	50	52	1	NM	4,445	0	0	18.0		
	09/23/05	20:00	NM	NA	2,890	NA	45	43	43	40	32	38	5	NM	3,000	0	0	17.9		
	09/24/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM		NA
	09/25/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM		NA
12	09/26/05	21:15	NM	NA	12,350	NA	54	51	47	42	34	43	4	NM	11,670	4	480	31.8	2.7	
	09/27/05	20:30	NM	NA	4,190	NA	50	47	45	43	40	43	2	NM	4,185	0	0	31.6		
	9/28/2005 <sup>(e)</sup>	19:15	0.3	NA	3,105	NA	60	60	55	50	44	51	4	6.0	2,755	0	0	31.5		
	09/29/05	19:30	3.2	2.9	3,255	19	52	50	43	40	32	40	3	5.5	3,840	3	360	31.3		
	09/30/05 <sup>(f)</sup>	21:30	6.1	2.9	5,345	31	50	50	45	42	40	43	2	1.0	3,850	2	250	31.0		
	10/01/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM		NA
10/02/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	NA		
13	10/03/05	21:30	15.8	9.7	14,010	24	60	57	54	50	50	52	2	0.0	12,880	7	890	30.3	2.6	
	10/04/05	21:30	18.9	3.1	4,493	24	55	52	50	46	44	49	1	3.0	4,060	3	390	30.1		
	10/05/05	23:30	21.0	2.1	4,377	35	65	60	57	56	52	55	2	1.0	4,175	1	170	29.9		
	10/06/05	18:30	23.7	2.7	2,313	14	60	56	55	40	42	50	5	3.0	2,295	0	0	29.8		
	10/07/05	18:30	26.2	2.5	3,617	24	45	43	43	38	38	37	6	10.0	3,350	1	80	29.6		
	10/08/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM		NA
	10/09/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM		NA
14	10/10/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	NA	
	10/11/05	18:45	38.1	11.9	17,050	24	50	48	42	38	36	38	4	9.0	15,975	7	870	28.8	2.6	
	10/12/05	17:15	40.9	2.8	3,900	23	64	60	57	54	53	54	3	2.5	3,503	3	380	28.6		
	10/13/05	20:00	43.9	3.0	4,280	24	50	47	44	38	36	38	6	9.0	3,862	3	390	28.4		
	10/14/05	20:00	47.2	3.3	4,870	25	50	49	45	40	40	40	5	2.5	4,500	2	250	28.2		
	10/15/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM		NA
10/16/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	NA		

**US EPA Arsenic Demonstration Project at BSLMHP, MN – Daily System Operation Log Sheet (continued)**

Week No.	Date	Time	New Well		Volume to Treatment		Pressure Tanks		Pressure Filtration					Volume to Distribution		Backwash		KMnO <sub>4</sub> Application	
			Hour Meter (hr)	Daily Operation (hr)	Daily Volume (gal)	Average Flowrate (gpm)	Pressure Tank 1 (psig)	Pressure Tank 2 (psig)	IN (psig)	TA/TB (psig)	TC/TD (psig)	OUT (psig)	ΔP Across System (psig)	Flowrate (gpm)	Daily Volume (gal)	No. of Tanks Backwashed	Wastewater Produced (gal)	KMnO <sub>4</sub> Tank Level (in)	Average KMnO <sub>4</sub> Dose (mg/L)
15	10/17/05	20:30	59.3	12.1	NA	NA	55	52	48	45	44	45	3	3.0	16,780	10	1,260	27.3	2.6
	10/18/05	20:15	62.5	3.2	NA	NA	58	54	51	43	42	45	6	7.5	4,390	2	260	27.0	
	10/19/05	20:15	66.1	3.6	5,625	26	65	60	56	52	50	52	4	2.5	5,195	2	250	26.8	
	10/20/05	21:30	70.5	4.4	6,975	26	50	48	52	48	45	46	6	NM	6,335	3	360	26.4	
	10/21/05	20:30	74.0	3.5	5,530	26	54	50	55	40	40	40	15	NM	5,055	2	250	26.2	
	10/22/05	NM	NM	NA	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	
10/23/05	NM	NM	NA	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	NA
16	10/24/05	20:00	82.4	8.4	13,260	26	65	60	56	52	50	50	6	5.0	12,265	4	520	25.5	2.5
	10/25/05	22:15	85.1	2.7	4,100	25	55	52	50	46	44	47	3	1.0	3,750	3	350	25.3	
	10/26/05	18:30	87.4	2.3	3,570	26	52	49	44	30	30	31	13	15.0	3,360	1	120	25.1	
	10/27/05	18:30	89.9	2.5	3,430	23	60	55	53	45	44	48	5	0.0	3,105	2	250	24.9	
	10/28/05	21:30	92.6	2.7	3,890	24	60	55	54	50	50	50	4	0.0	3,635	1	120	24.8	
	10/29/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	
10/30/05	NM	NM	NA	NA	NA	NA	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	NA	
17	10/31/05	18:30	100.5	7.9	11,440	24	55	50	48	45	44	46	2	0.0	10,480	5	610	24.3	3.0
	11/01/05	18:30	103.1	2.6	4,793	31	64	60	58	54	52	53	5	1.0	3,643	1	120	24.0	
	11/02/05	18:00	105.9	2.8	3,357	20	55	50	46	42	40	41	5	2.5	3,927	3	360	23.8	
	11/03/05	16:30	108.0	2.1	3,080	24	65	60	57	52	52	53	4	2.5	2,930	1	120	23.7	
	11/04/05	19:00	111.0	3.0	4,760	26	56	54	51	44	44	45	6	2.5	4,315	2	240	23.4	
	11/05/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	
11/06/05	NM	NM	NA	NA	NA	NA	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	NA	
18	11/07/05	18:30	117.5	6.5	10,057	26	60	55	48	44	44	45	3	2.5	8,826	5	690	NM	2.8
	11/08/05	17:00	120.8	3.3	4,836	24	54	50	46	38	38	40	6	6.0	4,749	1	140	22.6	
	11/09/05	19:30	124.4	3.6	5,449	25	65	60	57	48	48	50	7	8.0	5,050	3	360	22.3	
	11/10/05	21:15	127.8	3.4	5,168	25	55	45	41	40	39	40	1	2.5	4,640	2	240	22.1	
	11/11/05	23:15	130.4	2.6	4,081	26	56	54	51	45	44	46	5	1.0	3,705	2	240	21.9	
	11/12/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	
11/13/05	NM	NM	NA	NA	NA	NA	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	NA	
19	11/14/05	17:00	138.0	7.6	10,986	24	55	53	48	33	32	35	13	2.5	10,081	6	820	21.3	5.0
	11/15/05	18:00	141.0	3.0	4,743	26	55	50	47	42	42	40	7	6.0	4,209	2	240	20.9	
	11/16/05	18:30	144.3	3.3	5,648	29	55	49	53	50	50	49	4	5.0	5,095	3	380	20.4	
	11/17/05	18:00	146.8	2.5	3,782	25	63	60	58	54	54	55	3	1.0	3,470	1	130	20.0	
	11/18/05	17:30	149.5	2.7	4,226	26	63	60	56	54	52	55	1	0.0	3,860	2	250	19.6	
	11/19/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	
11/20/05	NM	NM	NA	NA	NA	NA	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	NA	
20	11/21/05	10:15	159.5	10.0	14,983	25	62	60	60	55	54	55	5	7.5	13,405	9	1,160	18.3	3.5
	11/22/05	18:00	162.9	3.4	5,391	26	65	62	58	54	53	55	3	5.0	4,805	3	390	18.0	
	11/23/05	21:00	167.3	4.4	7,070	27	65	60	58	52	52	55	3	7.5	6,240	5	640	17.5	
	11/24/05	17:30	169.8	2.5	3,665	24	58	60	52	50	48	50	2	1.0	3,250	2	260	17.3	
	11/25/05	18:30	173.4	3.6	5,928	27	55	50	42	40	40	38	4	1.5	5,330	2	250	NM	
	11/26/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	
11/27/05	NM	NM	NA	NA	NA	NA	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	NA	

**US EPA Arsenic Demonstration Project at BSLMHP, MN – Daily System Operation Log Sheet (continued)**

Week No.	Date	Time	New Well		Volume to Treatment		Pressure Tanks		Pressure Filtration					Volume to Distribution		Backwash		KMnO <sub>4</sub> Application			
			Hour Meter (hr)	Daily Operation (hr)	Daily Volume (gal)	Average Flowrate (gpm)	Pressure Tank 1 (psig)	Pressure Tank 2 (psig)	IN (psig)	TA/TB (psig)	TC/TD (psig)	OUT (psig)	ΔP Across System (psig)	Flowrate (gpm)	Daily Volume (gal)	No. of Tanks Backwashed	Wastewater Produced (gal)	KMnO <sub>4</sub> Tank Level (in)	Average KMnO <sub>4</sub> Dose (mg/L)		
21	11/28/05	17:00	183.2	9.8	15,655	27	55	52	46	41	40	40	6	1.0	14,115	8	1,020	29.6	4.8		
	11/29/05	18:30	187.2	4.0	5,872	24	55	50	46	42	40	42	4	3.0	5,230	3	370	29.1			
	11/30/05	14:30	189.9	2.7	4,010	25	54	50	44	40	39	40	4	1.0	3,350	4	490	28.8			
	12/01/05	18:00	193.8	3.9	6,390	27	55	50	41	39	38	39	2	7.5	5,855	2	250	28.3			
	12/02/05	21:00	197.9	4.1	6,161	25	54	50	44	40	40	41	3	1.5	5,250	4	510	27.8			
	12/03/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA		NM	NA
12/04/05	NM	NM	NA	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	NA		
22	12/05/05	21:30	210.0	12.1	18,880	26	55	50	41	38	36	37	4	3.0	16,870	11	1,390	26.0	5.1		
	12/06/05	20:00	213.1	3.1	4,700	25	54	50	49	42	42	45	4	5.0	4,345	1	130	25.6			
	12/07/05	19:00	216.7	3.6	5,966	28	54	50	44	39	36	37	7	3.0	5,445	2	250	25.1			
	12/08/05	13:00	219.0	2.3	4,068	29	65	60	57	52	50	52	5	3.0	3,220	4	480	24.7			
	12/09/05	18:00	224.1	5.1	8,590	28	64	60	56	51	50	52	4	6.0	7,310	5	700	23.9			
	12/10/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA		NM	NA
12/11/05	NM	NM	NA	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	NA		
23	12/12/05	18:00	235.4	11.3	16,425	24	64	60	59	56	54	55	4	3.0	15,230	7	970	22.3	5.4		
	12/13/05	19:30	239.4	4.0	5,975	25	55	50	48	46	44	45	3	5.0	5,500	2	250	21.7			
	12/14/05	19:30	242.8	3.4	4,790	23	65	60	56	52	50	52	4	2.5	4,360	1	120	21.3			
	12/15/05	18:00	246.3	3.5	4,624	22	65	60	55	49	47	49	6	4.0	4,170	3	370	20.6			
	12/16/05	07:12	249.4	3.1	4,651	25	55	50	40	30	30	30	10	10.0	4,200	2	210	20.4			
	12/17/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA		NM	NA
12/18/05	NM	NM	NA	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	NA		
24	12/19/05	21:00	266.2	16.8	26,100	26	55	48	45	39	38	40	5	6.0	23,690	10	1,320	17.8	5.4		
	12/20/05	18:00	270.9	4.7	7,760	28	59	55	53	48	47	48	5	7.5	6,970	4	470	17.0			
	12/21/05	19:00	277.3	6.4	9,970	26	62	56	53	48	47	48	5	4.0	8,900	5	590	30.6			
	12/22/05	19:30	281.7	4.4	6,250	24	60	60	59	52	52	54	5	4.0	5,690	3	350	30.0			
	12/23/05	NM	NM	NA	NA	NA	NM	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA		NM	NA
	12/24/05	NM	NM	NA	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA		NM	NA
12/25/05	NM	NM	NA	NA	NA	NA	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	NA		
25	12/26/05	18:30	300.8	19.1	29,172	25	54	50	42	37	36	37	5	5.0	25,740	14	1,770	27.4	6.1		
	12/27/05	18:00	304.9	4.1	6,770	28	65	60	55	43	42	45	10	5.0	4,900	4	470	26.8			
	12/28/05	19:15	309.7	4.8	5,908	21	54	50	45	40	38	40	5	3.0	5,925	3	350	26.1			
	12/29/05	19:30	313.5	3.8	5,570	24	54	47	44	40	39	40	4	2.0	4,845	3	350	25.6			
	12/30/05	19:00	316.9	3.4	4,650	23	55	45	42	40	40	40	2	3.0	2,320	1	140	25.2			
	12/31/05	NM	NM	NA	NA	NM	NM	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA		NM	NA
01/01/06	NM	NM	NA	NA	NM	NM	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	NA		
26	01/02/06	10:30	331.5	14.6	23,050	26	65	60	57	56	55	55	2	2.0	21,300	12	1,620	23.0	5.6		
	01/03/06 <sup>(9)</sup>	12:30	336.2	4.7	NA	NA	60	55	58	53	52	52	6	2.0	6,080	4	470	22.4			
	01/04/06	17:00	336.4	0.2	4,550	NA	65	59	55	52	50	50	5	3.0	3,940	3	350	21.9			
	01/05/06	10:00	341.2	4.8	7,365	26	56	53	50	44	44	45	5	2.5	6,130	4	460	21.1			
	01/06/06	19:30	345.8	4.6	7,290	26	55	52	48	40	40	40	8	7.5	6,000	4	470	20.5			
	01/07/06	NM	NM	NA	NA	NM	NM	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA		NM	NA
01/08/06	NM	NM	NA	NA	NM	NM	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	NM	NA		

**US EPA Arsenic Demonstration Project at BSLMHP, MN – Daily System Operation Log Sheet (continued)**

Week No.	Date	Time	New Well		Volume to Treatment		Pressure Tanks		Pressure Filtration					Volume to Distribution		Backwash		KMnO <sub>4</sub> Application	
			Hour Meter (hr)	Daily Operation (hr)	Daily Volume (gal)	Average Flowrate (gpm)	Pressure Tank 1 (psig)	Pressure Tank 2 (psig)	IN (psig)	TA/TB (psig)	TC/TD (psig)	OUT (psig)	ΔP Across System (psig)	Flowrate (gpm)	Daily Volume (gal)	No. of Tanks Backwashed	Wastewater Produced (gal)	KMnO <sub>4</sub> Tank Level (in)	Average KMnO <sub>4</sub> Dose (mg/L)
27	01/09/06	18:00	362.3	16.5	25,483	26	55	50	45	40	38	40	5	4.0	21,500	12	1,520	17.9	5.5
	01/10/06	17:00	366.4	4.1	6,060	25	65	60	55	51	52	53	2	1.0	4,835	5	690	17.3	
	01/11/06	17:00	370.5	4.1	6,400	26	65	60	59	52	50	52	7	12.0	5,495	2	250	31.0	
	01/12/06	19:15	376.1	5.6	8,635	26	54	50	43	39	38	38	5	5.0	7,125	5	650	30.2	
	01/13/06	19:00	380.5	4.4	6,385	24	55	50	45	38	36	38	7	3.0	5,465	3	380	29.6	
	01/14/06	NM	NM	NA	NM	NM	NM	NM	NM	NM	NM	NM	NM	NA	NM	NA	NM	NA	
28	1/16/2006 <sup>(b)</sup>	17:00	394.7	14.2	21,965	26	65	60	59	52	50	52	7	8.0	NA	13	1,640	27.6	5.9
	01/17/06	21:00	399.8	5.1	7,757	25	65	60	57	50	50	52	5	12.5	6,280	5	620	26.9	

Note:

- (a) On 08/09/05, both sets of duplex filters stuck in backwash mode due to sediment dislodged in purge/control valve, preventing it from closing. System bypassed.
- (b) On 08/09/06, a pressure gauge after each set of duplex filters installed.
- (c) On 08/11/05, pressure gauge on pressure tank 2 replaced.
- (d) On 09/21/05, two flow meters, one on treated water line and one on backwash discharge line, installed although readings not recorded until 09/28/05.
- (e) On 09/28/05 hour meter installed.
- (f) On 09/30/06, pressure gauge changed out for duplex units TC/TD.
- (g) On 01/03/06, totalizer to treatment re-set.
- (h) Totalizer to distribution re-set.

NM = not measured

NA = not available

**APPENDIX B**  
**ANALYTICAL DATA**

### Analytical Results from Long Term Sampling at BSLMHP, MN

Sampling Date		07/13/05			07/20/05			07/26/05			08/02/05			08/18/05 <sup>(a, b)</sup>			08/24/05			
Sampling Location		IN	AC	TT	IN	AC	TT	IN	AC	TA/TB	TC/TD									
Parameter	Unit																			
Stroke Length	%	33			33			33			33			26			26			
Alkalinity (as CaCO <sub>3</sub> )	mg/L	352	374	374	365	365	361	365	370	365	352	365	374	352	365	361	352	365	361	374
Fluoride	mg/L	0.2	0.2	0.2	-	-	-	-	-	-	-	-	-	0.2	0.2	0.2	-	-	-	-
Sulfate	mg/L	<1	<1	<1	-	-	-	-	-	-	-	-	-	<1	<1	<1	-	-	-	-
Nitrate (as N)	mg/L	0.1	0.1	0.3	-	-	-	-	-	-	-	-	-	<0.05	<0.05	<0.05	-	-	-	-
Orthophosphate (as PO <sub>4</sub> )	mg/L	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05
P (total) (as P)	mg/L	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Silica (as SiO <sub>2</sub> )	mg/L	23.3	23.3	22.7	24.7	24.4	24.2	23.5	23.6	23.9	23.8	24.0	23.6	24.1	24.2	23.9	29.4	28.6	28.4	28.2
Turbidity	NTU	25.0	3.1	0.6	23.0	2.8	0.5	25.0	2.9	0.1	26.0	4.7	11.0	33.0	3.7	0.4	24.0	2.9	0.7	0.2
TOC	mg/L	-	-	-	-	-	-	-	-	-	-	-	-	4.1	3.9	4.0	-	-	-	-
pH	S.U.		7.5	7.7	7.3	7.2	7.2	7.4	7.3	7.2	7.4	7.3	7.3	7.2	7.3	7.3	7.3	7.4	7.3	7.4
Temperature	°C	14.9	12.7	12.3	11.4	12.3	11.9	10.4	11.0	11.0	11.2	12.1	12.1	1.0	14.1	13.8	12.3	12.8	12.5	12.8
DO	mg/L	2.0	0.7	1.1	2.5	0.5	0.7	3.6	1.7	0.9	3.5	1.0	1.2	0.9	0.9	0.7	10.4	0.8	0.7	1.1
ORP	mV	-23	196	219	-29	85	144	-40	144	173	-35	154	196	-76	2	43	-48	138	159	181
Total Hardness (as CaCO <sub>3</sub> )	mg/L	383	330	329	-	-	-	-	-	-	-	-	-	320	317	323	-	-	-	-
Ca Hardness (as CaCO <sub>3</sub> )	mg/L	228	197	197	-	-	-	-	-	-	-	-	-	188	190	187	-	-	-	-
Mg Hardness (as CaCO <sub>3</sub> )	mg/L	155	133	132	-	-	-	-	-	-	-	-	-	131	128	137	-	-	-	-
As (total)	µg/L	36.4	29.6	4.3	34.7	26.7	17.7	26.6	24.8	5.5	25.7	23.0	8.0	26.4	23.2	5.1	30.4	31.5	3.5	3.3
As (soluble)	µg/L	30.3	3.3	3.0	-	-	-	-	-	-	-	-	-	26.2	4.8	4.8	-	-	-	-
As (particulate)	µg/L	6.1	26.3	1.3	-	-	-	-	-	-	-	-	-	0.2	18.4	0.3	-	-	-	-
As (III)	µg/L	13.9	1.6	1.7	-	-	-	-	-	-	-	-	-	24.1	2.6	3.4	-	-	-	-
As (V)	µg/L	16.5	1.7	1.3	-	-	-	-	-	-	-	-	-	2.1	2.2	1.4	-	-	-	-
Fe (total)	µg/L	3,315	3,173	157	2,786	2,766	482	2,864	2,704	45	2,964	2,578	666	2,895	2,773	<25	2,764	2,706	<25	<25
Fe (soluble)	µg/L	2,792	<25	<25	-	-	-	-	-	-	-	-	-	2,954	<25	<25	-	-	-	-
Mn (total)	µg/L	154	996	428	139	634	561	137	844	727	135	1,126	487	139	1,097	1,010	130	871	475	467
Mn (soluble)	µg/L	133	377	391	-	-	-	-	-	-	-	-	-	142	850	1,000	-	-	-	-

(a) Onsite water quality parameters taken on 08/17/05. (b) System bypassed on 08/09/05 and samples not collected that week.

**Analytical Results from Long Term Sampling at BSLMHP, MN (continued)**

Sampling Date		08/31/05 <sup>(a)</sup>				09/07/05 <sup>(b)</sup>				09/14/05				09/20/05			09/27/05 <sup>(c)</sup>			
Sampling Location		IN	AC	TA/TB	TC/TD	IN	AC	TA/TB	TC/TD	IN	AC	TA/TB	TC/TD	IN	AC	TT	IN	AC	TA/TB	TC/TD
Parameter	Unit																			
Stroke Length	%	15				15				26				26			26			
Alkalinity (as CaCO <sub>3</sub> )	mg/L	383	370	374	374	361	365	361	365	356	370	370	352	374	374	370	378	374	374	374
Fluoride	mg/L	-	-	-	-	-	-	-	-	-	-	-	-	0.2	0.2	0.2	-	-	-	-
Sulfate	mg/L	-	-	-	-	-	-	-	-	-	-	-	-	<1	<1	<1	-	-	-	-
Nitrate (as N)	mg/L	-	-	-	-	-	-	-	-	-	-	-	-	<0.05	<0.05	<0.05	-	-	-	-
Orthophosphate (as PO <sub>4</sub> )	mg/L	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05	<0.05
P (total) (as P)	mg/L	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
Silica (as SiO <sub>2</sub> )	mg/L	25.8	25.6	25.8	25.8	24.1	24.3	24.0	24.2	22.6	22.9	22.5	22.7	22.6	22.5	22.2	25.7	25.7	25.6	25.3
Turbidity	NTU	32.0	5.3	4.2	4.2	13.0	6.0	14.0	14.0	32.0	3.4	0.2	0.3	31.0	3.4	0.5	32.0	4.1	<0.1	<0.1
TOC	mg/L	-	-	-	-	-	-	-	-	-	-	-	-	4.8	4.6	4.8	-	-	-	-
pH	S.U.	NA	NA	NA	NA	7.3	7.4	7.3	7.5	7.3	7.2	7.2	7.2	7.2	7.3	7.2	7.4	7.4	7.4	7.4
Temperature	°C	NA	NA	NA	NA	10.8	11.3	10.7	11.5	11.5	10.9	11.2	10.7	10.7	13.4	13.6	9.5	9.8	9.9	10.0
DO	mg/L	NA	NA	NA	NA	0.9	0.5	0.9	0.7	1.5	0.7	0.5	0.5	0.7	1.0	0.9	0.8	1.6	0.7	0.7
ORP	mV	NA	NA	NA	NA	-63	-22	-9	-12	-49	101	96	101	-66	18	6	-54	1	6	8
Total Hardness (as CaCO <sub>3</sub> )	mg/L	-	-	-	-	-	-	-	-	-	-	-	-	307	307	306	-	-	-	-
Ca Hardness (as CaCO <sub>3</sub> )	mg/L	-	-	-	-	-	-	-	-	-	-	-	-	177	178	176	-	-	-	-
Mg Hardness (as CaCO <sub>3</sub> )	mg/L	-	-	-	-	-	-	-	-	-	-	-	-	131	129	130	-	-	-	-
As (total)	µg/L	27.0	27.9	13.8	12.3	20.6 <sup>(g)</sup>	28.8	21.5	17.5	23.7	24.8	2.8	4.7	27.4	27.1	2.9	26.7	25.4	8.4	7.6
As (soluble)	µg/L	-	-	-	-	-	-	-	-	-	-	-	-	27.6	4.7	3.2	-	-	-	-
As (particulate)	µg/L	-	-	-	-	-	-	-	-	-	-	-	-	<0.1	22.4	<0.1	-	-	-	-
As (III)	µg/L	-	-	-	-	-	-	-	-	-	-	-	-	25.6	1.7	1.5	-	-	-	-
As (V)	µg/L	-	-	-	-	-	-	-	-	-	-	-	-	2.0	3.1	1.7	-	-	-	-
Fe (total)	µg/L	2,888	3,096	571	465	1069	2,619	1,052	1,140	2,716	2,795	<25	78	3,094	2,911	<25	2,934	2,796	<25	<25
Fe (soluble)	µg/L	-	-	-	-	-	-	-	-	-	-	-	-	2,883	<25	<25	-	-	-	-
Mn (total)	µg/L	133	581	906	865	430	416	447	430	131	1,042	651	897	149	883	616	141	676	802	841
Mn (soluble)	µg/L	-	-	-	-	-	-	-	-	-	-	-	-	145	533	634	-	-	-	-

(a) Operator not able to take onsite water quality parameters due to busy work schedule. (b) Onsite water quality parameters taken on 09/06/05. (c) Onsite water quality parameters taken on 09/28/05.

**Analytical Results from Long Term Sampling at BSLMHP, MN (continued)**

Sampling Date		10/05/05 <sup>(a)</sup>				10/12/05 <sup>(b)</sup>				10/19/05 <sup>(c)</sup>			10/26/05 <sup>(d)</sup>				11/02/05 <sup>(e)</sup>				
Sampling Location		IN	AC	TA/TB	TC/TD	IN	AC	TA/TB	TC/TD	IN	AC	TT	IN	AC	TA/TB	TC/TD	IN	AC	TA/TB	TC/TD	
Parameter	Unit																				
Stroke Length	%	26				26				26			26				26				
Alkalinity (as CaCO <sub>3</sub> )	mg/L	356	321	352	374	365 365	374 370	374 374	365 365	383	378	383	352	365	361	361	361	352	356	352	352
Fluoride	mg/L	-	-	-	-	-	-	-	-	0.2	0.2	0.2	-	-	-	-	-	-	-	-	
Sulfate	mg/L	-	-	-	-	-	-	-	-	<1	<1	<1	-	-	-	-	-	-	-	-	
Nitrate (as N)	mg/L	-	-	-	-	-	-	-	-	<0.05	<0.05	<0.05	-	-	-	-	-	-	-	-	
Orthophosphate (as PO <sub>4</sub> )	mg/L	<0.05	<0.05	<0.05	<0.05	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	
P (total) (as P)	mg/L	0.5	0.5	0.02	0.02	0.5 0.5	0.4 0.5	0.1 0.03	0.03 0.1	0.5	0.5	0.1	0.5	0.5	0.03	0.03	0.5	0.1	0.04	0.04	
Silica (as SiO <sub>2</sub> )	mg/L	23.1	22.6	23.6	25.6	23.2 23.3	23.6 23.6	23.2 23.3	23.2 23.0	23.0	23.2	21.7	24.5	25.1	24.1	24.5	24.7	24.5	24.0	23.9	
Turbidity	NTU	28.0	4.6	1.2	<0.1	34.0 34.0	3.0 3.3	0.4 0.5	0.5 0.5	34.0	4.0	1.3	33.0	3.3	0.2	1.3	33.0	3.1	0.1	0.3	
TOC	mg/L	-	-	-	-	-	-	-	-	3.7	3.3	3.8	-	-	-	-	-	-	-	-	
pH	S.U.	7.4	7.5	7.4	7.5	7.4	7.4	7.4	7.4	7.4	7.4	7.3	7.3	7.4	7.4	7.4	7.4	7.4	7.4	7.4	
Temperature	°C	10.0	10.0	10.0	10.0	10.5	10.2	10.3	10.3	10.8	10.8	10.8	10.6	10.5	10.5	10.6	10.0	10.1	10.1	10.2	
DO	mg/L	0.9	1.5 <sup>(e)</sup>	1.2 <sup>(e)</sup>	1.3 <sup>(e)</sup>	0.7	1.1	0.8	0.8	0.8	1.0	0.7	1.1	1.3	1.1	1.0	0.7	0.7	1.0	0.8	
ORP	mV	-64	175	177	183	-58	28	35	45	-56	23	29	-50	-1	28	33	-30	55	71	78	
Total Hardness (as CaCO <sub>3</sub> )	mg/L	-	-	-	-	-	-	-	-	315	315	313	-	-	-	-	-	-	-	-	
Ca Hardness (as CaCO <sub>3</sub> )	mg/L	-	-	-	-	-	-	-	-	188	189	184	-	-	-	-	-	-	-	-	
Mg Hardness (as CaCO <sub>3</sub> )	mg/L	-	-	-	-	-	-	-	-	128	126	129	-	-	-	-	-	-	-	-	
As (total)	µg/L	22.8	21.8	3.2	3.3	27.2 28.7	25.8 27.6	6.3 5.8	6.3 10.1	29.1	27.8	4.2	26.0	26.6	6.4	5.8	25.1	5.6	5.6	4.2	
As (soluble)	µg/L	-	-	-	-	-	-	-	-	25.2	4.0	2.9	-	-	-	-	-	-	-	-	
As (particulate)	µg/L	-	-	-	-	-	-	-	-	3.8	23.8	1.3	-	-	-	-	-	-	-	-	
As (III)	µg/L	-	-	-	-	-	-	-	-	20.8	0.9	0.8	-	-	-	-	-	-	-	-	
As (V)	µg/L	-	-	-	-	-	-	-	-	4.5	3.1	2.4	-	-	-	-	-	-	-	-	
Fe (total)	µg/L	2,596	2,523	<25	<25	2,820 2,874	2,562 2,707	142 74	72 547	2,680	2,624	136	2,979	2,968	<25	67	3,758	247	62	48	
Fe (soluble)	µg/L	-	-	-	-	-	-	-	-	2,594	<25	<25	-	-	-	-	-	-	-	-	
Mn (total)	µg/L	119	760	600	628	128 130	791 827	687 694	794 838	128	953	548	134	888	852	846	176	984	988	952	
Mn (soluble)	µg/L	-	-	-	-	-	-	-	-	132	468	535	-	-	-	-	-	-	-	-	

(a) Onsite water quality parameters taken on 10/06/05. (b) Duplicate sampling week. (c) Onsite water quality parameters taken on 10/18/05. (d) Onsite water quality parameters taken on 10/27/05. (e) Onsite water quality parameters taken on 11/01/05.

### Analytical Results from Long Term Sampling at BSLMHP, MN (continued)

Sampling Date		11/09/05				11/15/05 <sup>(a,b)</sup>			11/29/05 <sup>(c)</sup>				12/08/05 <sup>(d)</sup>				12/14/05 <sup>(e)</sup>			
Sampling Location		IN	AC	TA/TB	TC/TD	IN	AC	TT	IN	AC	TA/TB	TC/TD	IN	AC	TA/TB	TC/TD	IN	AC	TA/TB	TC/TD
Parameter	Unit																			
Stroke Length	%	26				40			38				40				40			
Alkalinity (as CaCO <sub>3</sub> )	mg/L	370	370	365	370	352	365	370	352	370	361	356	374	374	370	370	374	365	378	378
Fluoride	mg/L	-	-	-	-	0.2	0.2	0.2	-	-	-	-	0.2	0.2	0.2	0.2	-	-	-	-
Sulfate	mg/L	-	-	-	-	<1	<1	<1	-	-	-	-	<1	<1	<1	<1	-	-	-	-
Nitrate (as N)	mg/L	-	-	-	-	<0.05	<0.05	<0.05	-	-	-	-	<0.05	<0.05	<0.05	<0.05	-	-	-	-
Orthophosphate (as PO <sub>4</sub> )	mg/L	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
P (total) (as P)	mg/L	0.5	0.5	0.1	0.1	0.5	0.5	0.2	0.5	0.5	0.4	0.1	0.4	0.4	0.02	0.02	0.5	0.5	0.2	0.2
																	0.6	0.6	0.2	0.2
Silica (as SiO <sub>2</sub> )	mg/L	23.9	23.6	24.0	24.0	23.5	23.7	23.7	24.3	24.6	24.7	25.0	23.5	23.9	23.9	23.8	25.4	25.6	25.1	25.8
																	26.1	26.4	25.5	24.9
Turbidity	NTU	33.0	3.2	0.1	0.7	34.0	3.2	0.9	32.0	4.2	1.3	0.5	26.0	3.9	0.1	0.5	34.0	5.1	0.7	1.9
																	35.0	5.2	0.8	1.2
TOC	mg/L	-	-	-	-	NA	NA	NA	-	-	-	-	NA	NA	NA	NA	-	-	-	-
pH	S.U.	7.4	7.4	7.4	7.4	7.3	7.3	7.2	7.3	7.3	7.3	7.3	7.3	7.3	7.3	7.3	7.3	7.3	7.3	7.3
Temperature	°C	10.0	10.2	10.2	10.4	9.4	9.5	9.5	9.8	9.6	9.6	9.7	9.6	9.4	9.3	9.4	9.3	9.5	9.3	9.2
DO	mg/L	0.9	0.8	0.9	0.8	1.3	1.0	1.0	1.2	1.6	0.9	1.0	1.1	1.1	0.9	1.1	1.2	1.1	1.6	0.9
ORP	mV	-38	39	65	68	-39	62	76	-39	55	65	71	-42	54	65	68	-26	52	59	64
Total Hardness (as CaCO <sub>3</sub> )	mg/L	-	-	-	-	311	321	338	-	-	-	-	296	295	304	307	-	-	-	-
Ca Hardness (as CaCO <sub>3</sub> )	mg/L	-	-	-	-	186	192	212	-	-	-	-	184	182	185	185	-	-	-	-
Mg Hardness (as CaCO <sub>3</sub> )	mg/L	-	-	-	-	125	129	126	-	-	-	-	112	114	119	122	-	-	-	-
As (total)	µg/L	36.6	36.1	11.3	5.7	33.2	34.1	17.1	30.3	34.1	29.8	9.2	24.2	24.9	2.0	2.1	26.4	25.6	12.1	12.6
																	27.6	25.6	11.3	12.4
As (soluble)	µg/L	-	-	-	-	28.8	8.7	6.2	-	-	-	-	24.4	2.7	2.0	2.0	-	-	-	-
As (particulate)	µg/L	-	-	-	-	4.4	25.4	10.9	-	-	-	-	<0.1	22.2	<0.1	0.1	-	-	-	-
As (III)	µg/L	-	-	-	-	27.4	5.4	4.4	-	-	-	-	24.5	0.3	0.3	0.4	-	-	-	-
As (V)	µg/L	-	-	-	-	1.4	3.3	1.7	-	-	-	-	<0.1	2.4	1.6	1.6	-	-	-	-
Fe (total)	µg/L	2,549	2,425	336	68	2,774	2,830	1,067	2,793	2,761	2,363	532	2,258	2,247	<25	<25	2,655	2,564	983	1,001
																	2,832	2,558	978	1,023
Fe (soluble)	µg/L	-	-	-	-	2,873	306	41	-	-	-	-	2,263	<25	<25	<25	-	-	-	-
Mn (total)	µg/L	117	1,031	951	971	130	1,004	1,091	124	1,123	1,002	432	110	1,037	203	187	123	1,242	611	665
																	125	1,243	611	673
Mn (soluble)	µg/L	-	-	-	-	138	946	1,062	-	-	-	-	110	166	202	190	-	-	-	-

(a) TOC samples broke during transit to laboratory. (b) Onsite water quality parameters taken 11/16/06. (c) Onsite water quality parameters taken on 11/30/05. (d) TOC samples out of hold time. (e) Onsite water quality parameters taken on 12/15/05.

**Analytical Results from Long Term Sampling at BSLMHP, MN (continued)**

Sampling Date		01/05/06 <sup>(a)</sup>			01/10/06 <sup>(b)</sup>				01/17/06 <sup>(c)</sup>			
Sampling Location		IN	AC	TT	IN	AC	TA/TB	TC/TD	IN	AC	TA/TB	TC/TD
Parameter	Unit											
Stroke Length	%	40			40				40			
Alkalinity (as CaCO <sub>3</sub> )	mg/L	378	383	378	374	378	378	383	383	378	378	378
Fluoride	mg/L	0.2	0.2	0.2	-	-	-	-	-	-	-	-
Sulfate	mg/L	<1	<1	<1	-	-	-	-	-	-	-	-
Nitrate (as N)	mg/L	<0.05	<0.05	<0.05	-	-	-	-	-	-	-	-
Orthophosphate (as PO <sub>4</sub> )	mg/L	-	-	-	-	-	-	-	-	-	-	-
P (total) (as P)	mg/L	0.5	0.4	0.1	0.4	0.4	<0.01	<0.01	0.5	0.5	0.03	0.03
Silica (as SiO <sub>2</sub> )	mg/L	24.9	25.3	24.7	24.4	24.2	23.8	24.2	25.3	25.4	24.1	24.7
Turbidity	NTU	31.0	5.8	1.4	31.0	4.3	0.2	4.6	32.0	6.5	0.3	3.3
TOC	mg/L	3.2	3.1	3.0	-	-	-	-	3.1	2.9	2.8	2.8
pH	S.U.	7.3	7.4	7.3	7.3	7.3	7.3	7.3	7.3	7.3	7.3	7.3
Temperature	°C	9.7	10.0	9.8	9.8	9.6	10.0	9.8	9.6	9.8	9.8	10.1
DO	mg/L	0.9	1.0	1.0	0.9	1.2	0.9	1.0	1.0	1.1	1.0	0.9
ORP	mV	-42	58	68	-38	62	57	61	-45	59	55	57
Total Hardness (as CaCO <sub>3</sub> )	mg/L	305	316	318	-	-	-	-	-	-	-	-
Ca Hardness (as CaCO <sub>3</sub> )	mg/L	190	195	193	-	-	-	-	-	-	-	-
Mg Hardness (as CaCO <sub>3</sub> )	mg/L	114	121	125	-	-	-	-	-	-	-	-
As (total)	µg/L	25.9	24.9	3.9	24.6	24.0	3.0	4.8	25.6	25.9	2.8	2.5
As (soluble)	µg/L	26.2	2.8	2.2	-	-	-	-	-	-	-	-
As (particulate)	µg/L	<0.1	22.1	1.7	-	-	-	-	-	-	-	-
As (III)	µg/L	25.0	0.4	0.4	-	-	-	-	-	-	-	-
As (V)	µg/L	1.2	2.4	1.7	-	-	-	-	-	-	-	-
Fe (total)	µg/L	2,737	2,566	194	2,581	2,629	28	307	2,593	2,427	27	<25
Fe (soluble)	µg/L	2,474	<25	<25	-	-	-	-	-	-	-	-
Mn (total)	µg/L	125	1,506	331	135	1,235	324	366	130	1,031	220	201
Mn (soluble)	µg/L	121	108	138	-	-	-	-	-	-	-	-

(a) Onsite water quality parameters taken on 01/04/06. (b) Onsite water quality parameters taken on 01/11/06. (c) Onsite water quality parameters taken on 01/17/06.